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AP-42 Section	11.1
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Report Sect.	4
Reference	45

VOL. I

RAMCON

ENVIRONMENTAL CORPORATION

AIR POLLUTION SOURCE TESTING AT

LEHMAN ROBERTS COMPANY
Memphis, Tennessee

VOLUME I

Submitted to:

LEHMAN ROBERT COMPANY
P.O. Box 666
Memphis, Tennessee 38101

and

NATIONAL ASPHALT PAVEMENT ASSOCIATION
5100 Forbes Boulevard
NAPA Building
Lanham, Maryland 20706-4413

Submitted on:

October 23, 1991

Submitted by:

RAMCON ENVIRONMENTAL CORPORATION
223 Scott Street
Memphis, Tennessee 38112
901/458-7000

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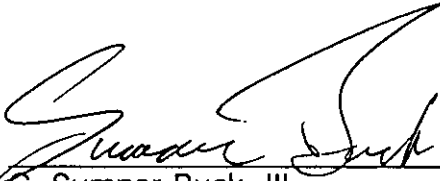
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CERTIFICATION

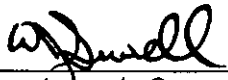
We do hereby certify that the following report has been reviewed and is to the best of our knowledge a true representation of the results. Further, all tests, sampling and analytical methods were performed in accordance with acceptable procedures to the United States Environmental Protection Agency.



G. Sumner Buck, III
President

10-23-91

Date



Wm. Joseph Sewell, II
Chemical Engineer

10/23/91

Date

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I. INTRODUCTION

On September 3 and 4 and October 1, 1991, personnel from RAMCON Environmental Corporation conducted source emissions determinations at Lehman Roberts Asphalt located in Memphis, Tennessee. The testing was conducted according to the National Asphalt Pavement Association (NAPA) guidelines entitled, "Protocol for Air Pollution Source Testing".

The scope of work involved testing this facility for filterable and condensable particulate matter, formaldehyde, and polynuclear aromatic hydrocarbons. These compounds were sampled according to specified isokinetic testing procedures. Also, "real-time" continuous emissions monitor (CEM) instrumentation was utilized to conduct on-site analysis for oxygen, carbon dioxide, total volatile organics, sulfur dioxide, carbon monoxide, and nitrogen oxides. Methane, benzene, toluene, ethyl benzene, and xylene compounds were analyzed on a semi-continuous basis by employing a gas chromatograph to the sampling location.

Additionally, stack gas moisture, velocity, and volumetric flow rates were determined to provide data enabling conversion of flue gas concentrations to emission data. These determinations were conducted in conjunction with each of the isokinetic testing procedures.

Where possible, the testing was conducted simultaneously. This provides correlations of the various stack effluents relationships with one another. Three (3) test runs were conducted for each testing procedure. Each test run was performed for a one hour duration.

The purpose of the testing project was to provide air emissions information for developing a database of information using various types of hot mix asphalt plants.

Mr. Tim Huey, Laboratory Technician of RAMCON Environmental Corporation, was responsible for the particulate laboratory analysis including taring the beakers and filters and recording final data in the laboratory record books. Custody of the particulate samples were limited to Mr. Huey and Mr. Crook. Triangle Laboratories,

Inc. of Durham, North Carolina conducted the PAH analysis. American Interplex of Little Rock, Arkansas conducted the formaldehyde analysis.

RAMCON Environmental's testing teams consisted of Ken Allmendinger; Field Supervisor and responsible for calibration of the instruments, Ray Jenkins; responsible for operating the gas chromatograph, Charles Crook; responsible for conducting the PM, CPM and PAH testing, and Billy Lockett; responsible for conducting the formaldehyde testing.

II. TEST RESULTS

Tables I - VI summarize the test results. Tables I & II summarize the instrumental gaseous concentrations and emissions summary. Table III shows the particulate results, Table IV the methane and BTEX concentrations, Table V the PAH results, and Table VI the formaldehyde test summary.

TABLE I
INSTRUMENTAL TEST SUMMARY
GASEOUS CONCENTRATIONS

<u>Run #</u>	<u>THC, ppm</u>	<u>SO₂, ppm</u>	<u>CO₂, %</u>	<u>CO, ppm</u>	<u>O₂, %</u>	<u>NO_x, ppm</u>
1	231.3	1.6	7.7	>1,000.0	7.3	45.6
2	252.1	2.3	7.1	>1,000.0	7.9	37.6
3	335.0	2.0	7.1	>1,000.0	7.9	39.3
Avg.	272.8	1.98	7.30	>1,000.0	7.7	40.8

TABLE II
EMISSIONS SUMMARY
LBS/HR

<u>Run</u>	<u>THC as methane</u>	<u>SO₂</u>	<u>CO</u>	<u>NO_x</u>
1	12.05	0.33	> 91.01	6.82
2	14.77	0.54	>102.33	6.32
3	20.36	0.49	>106.15	6.85
Avg.	15.73	0.45	> 99.83	6.66

TABLE III
PARTICULATE TEST SUMMARY
CONCENTRATION

<u>Run</u>	<u>Particulate Gr/DSCF</u>	<u>Particulate g/DSCM</u>	<u>CPM* gr/DSCF</u>	<u>CPM g/DSCM</u>
1	0.0067	0.0154	0.0024	0.0055
2	0.0142	0.0326	0.0021	0.0048
3	0.0133	0.0305	0.0013	0.0030
Avg.	0.0114	0.0262	0.0019	0.0044

*CPM = Condensable Particulate Matter

PARTICULATE EMISSIONS SUMMARY

<u>Run #</u>	<u>Particulate Lbs/Hr</u>	<u>CPM Lbs/Hr</u>
1	1.37	0.49
2	2.72	0.40
3	2.66	0.26
Avg.	2.25	0.38

TABLE IV
METHANE & BTEX TEST SUMMARY
PPM CONCENTRATIONS

<u>Run #</u>	<u>Methane</u>	<u>Benzene</u>	<u>Toluene</u>	<u>Ethyl Benzene</u>	<u>Xylene(s)</u>
1	11.25	*BDL	BDL	BDL	BDL
2	11.28	0.28	BDL	BDL	BDL
3	37.85	0.69	BDL	BDL	BDL
Avg.	20.13	0.32	BDL	BDL	BDL

*Below Detection Limit

TABLE V
PAH TEST SUMMARY

<u>Run #</u>	<u>Concentration Gr/DSCF</u>	<u>Emissions Lbs/Hr</u>
1	0.000272	0.049
2	0.000245	0.049
3	0.000273	0.057
Avg.	0.000263	0.052

TABLE VI
FORMALDEHYDE TEST SUMMARY

<u>Run #</u>	<u>Concentration Gr/DSCF</u>	<u>Emissions Lbs/Hr</u>
1	0.0029	0.62
2	0.0034	0.71
3	0.0003	0.06
Avg.	0.0022	0.46

III. SAMPLING & ANALYTICAL PROCEDURES

A. Total Particulate - US EPA Reference Method 5:

1. Preparation - All glassware utilized in each sampling train was thoroughly cleaned and dried prior to each test series. A glass fiber filter was used that had been labeled, desiccated for a minimum of 24 hours and pre-weighed.

The impinger system configuration was assembled using the outlined procedure in Method 5. One hundred ml of deionized water was placed in the first two impingers. The third impinger was initially empty and the fourth impinger contained a pre-weighed amount of silica gel for complete moisture removal. In assembling the sample train, a small amount of silicon grease was placed on the ball joints to ensure adequate sealing.

A stainless steel probe liner and nozzle system was utilized for the total particulate determinations. The probe housed a set of calibrated S-type pitot tubes and a calibrated thermocouple for monitoring stack temperature.

2. Sampling - The sample box was heated to an approximate temperature of 250°F. These temperatures were monitored throughout the testing. An ice bath was prepared to submerge the impinger system. The temperature of the last impinger was monitored throughout the testing to ensure adequate condensation of the water vapor in the flue gases.

A leak check was performed prior to each test run. The entire sample train system was subjected to a vacuum that did not exceed 0.02 cfm leakage rate. The vacuum established during the pre-test leak check was not exceeded during the test period.

Three sample runs were conducted at the sampling location to constitute a complete test. The sampling time was a minimum of 1 hour and at least 30 scf of stack gas was extracted via the sampling system.

When a test run was completed, a post-test leak check was conducted prior to any dismantling of the sampling train. Once this was successfully achieved, the sample train was dismantled for sample recovery.

The probe and connecting glassware were washed with acetone. The contents of the impingers were also volumetrically measured for moisture gain and transferred to a labeled sample container. The glass fiber filter was carefully transferred to its sample container.

3. Analysis - The glass fiber filter were desiccated for 24 hours prior to any weighing. The first weighing was performed after this initial period of drying. After a minimum of 6 additional hours of desiccating, a second weighing was conducted. The weights must agree within 0.0005 g. All analysis data was recorded. Sample field blanks of acetone were collected, contained, labeled and analyzed in conjunction with the samples.

B. Determination of Sulfur Dioxide Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 6C:

1. Calibration - The calibration of the instruments was performed using certified gas standards composed of a known concentration of sulfur dioxide in zero grade nitrogen. These gas standards were prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes an ultraviolet nondispersive infrared detector. The detection limitation is 0.1 ppm. Two test ranges are available according to the sulfur dioxide levels present in the gas stream. A 100 ppm and a 1000 ppm full-scale may be utilized. In this project, the burner was utilizing natural gas as a fuel and subsequent sulfur dioxide levels were very low or non-detectable.

Immediately prior to each compliance test series, a complete calibration of the instrument was performed. Each instrument had zero grade nitrogen injected into it and the zero potentiometer was adjusted, if necessary, until the proper voltage output from the analyzer was achieved.

Then a high range pollutant gas mixture, that has been prepared in the specified range percentage of the span or full-scale, is injected. After the system stabilizes, the span or full-scale potentiometer was adjusted until the voltage output from analyzer corresponds to the certification of analysis for the respective calibration gas.

When this procedure is complete and the system has responded properly to a zero and full-scale reading, a mid range certified calibration gas is injected into the system. No adjustments are made to the system except to achieve proper flow rate through the analyzer. The analyzer, after reaching a stable value, must correspond to the certified value of the calibration gas within a specified percentage of the full-scale.

This mid range calibration gas serves two purposes of quality control and quality assurance. The first is to show the instrument analyzes and outputs data on a linear scale. The second purpose is to validate that the zero and full-scale values of the instrument are properly set.

2. Sampling - After calibration, the system is purged with zero grade nitrogen to remove any pollutants that were injected as calibration gas. Once the system indicates that the pollutant gases have been removed, the calibration valve assembly is positioned to allow stack gas to flow through the instrument.

The sample gas is filtered at the stack position to remove any particulate matter. This prevents instruments from being contaminated and ensures reliable data acquisition.

All samples injected to the instruments are removed from the stack and delivered to the instruments via a heated probe and sample line. This prevents any condensation of water vapor and/or pollutant in the gas stream.

Three test runs were conducted to determine the concentration levels of sulfur dioxide. The test runs were conducted over a period of one hour.

To demonstrate the instrument did not exhibit any deviation from the calibrated values set at the beginning of a test period, a sample of certified calibration gas is injected into the sampling system at the conclusion of each test run. The sample system must respond within specified tolerance limits according to the initial system bias check.

This post-test calibration serves two purposes: 1) it demonstrates that excessive calibration drift of the instrument(s) did not occur during the test period and, 2) that the system was not contaminated with any foreign material from the source to alter any results during the test period.

C. Determination of Nitrogen Oxides Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 7E:

1. Calibration - The calibration of the instruments was performed using certified gas standards composed of a known concentration of nitrogen oxide in zero grade nitrogen. These gas standards were prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes a chemiluminescent detector. The detection limitation of the analyzer is 0.1 ppm. Multiple full-scale ranges are available for operation. A 250, 1000, 2500, and 10,000 ppm full-scale may be selected

according to the concentrations of NO_x present in the gas stream. The concentrations encountered at the Lehman Roberts hot mix facility were such that the 250 ppm scale was sufficient for bracketing the concentrations.

The initial calibration of the instruments was performed as previously mentioned in the sulfur dioxide section. A zero nitrogen and a high range calibration gas is utilized to set the instrument potentiometers for proper output.

2. Sampling - After calibration, the system is purged with zero grade nitrogen to remove any pollutants that were injected as calibration gas. Once the system indicates that the pollutant gases have been removed, the calibration valve assembly is positioned to allow stack gas to flow through the instrument.

Three test runs were conducted to determine the NO_x concentrations in the gas stream. Each test run will be conducted over a period of one hour.

To demonstrate that the instrument did not exhibit any deviation from the calibrated values set at the beginning of a test period, a sample of certified calibration gas is injected into the sampling system at the conclusion of each test run as in the sulfur dioxide testing. The sample system must respond within specified tolerance limits according to the initial system bias check.

D. Determination of Carbon Monoxide Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 10:

1. Calibration - The calibration of the instruments is performed using certified gas standards composed of a known concentration of carbon monoxide in zero grade nitrogen. These gas standards are prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis

certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes a Luft-type nondispersive infrared detector. The detection limitation of the analyzer is 0.1 ppm. Two full-scale ranges are available on the analyzer. A 500 ppm and a 1000 ppm full-scale may be utilized. The carbon monoxide levels encountered were analyzed using the 1000 ppm scale.

The initial calibration of the instrument is according to the procedure outlined above. Method 10, however, utilizes an additional calibration mixture for the calibration. A low level calibration gas is required in conjunction with the high and mid level calibration standards.

2. Sampling - Three (3) test runs were conducted to determine the emission value of CO. Each test run was conducted over a period of 1 hour .

To demonstrate that the instrument did not exhibit any deviation from the calibrated values set at the beginning of a test period, a sample of certified calibration gas is injected into the sampling system at the conclusion of each test run. The sample system must respond within specified tolerance limits according to the initial system bias check.

E. Determination of Gaseous Organic Emissions From Stationary Sources By Gas Chromatography - US EPA Method 18:

This procedure utilizes the technology of gas chromatography to separate, identify, and quantify various volatile organic compounds that co-exist in a flue gas stream. In this testing project, methane and the BTEX compounds were targeted.

The gas chromatograph was first conditioned in the laboratory where ideal conditions exist for this initial calibration. This consists of conditioning the column, if necessary, and creating calibration curves based on actual data

from the GC with known concentration standards. As required by EPA, three (3) standards-of known concentration were used in creating the calibration curves. The concentrations of the standards bracketed the expected concentration of pollutant at the source level.

A field calibration check was performed prior to introducing any sample into the gas chromatograph. This is performed by injecting one of the known standards into the GC and comparing the result to the calibration curve. It must agree within 5% of the previously determined response.

Analysis of the samples follow a successful field calibration. Collecting the sample consisted of extracting the sample from the stack via a heated sample line. The sample was introduced directly into the sample loop, where it was injected to the instrument for analysis.

Three test runs were performed to determine the values of the specified organic compounds. Each test run consisted of semi-continuously analyzing the gas stream for a one hour period.

F. Determination of Total Gaseous Organic Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 25A:

1. Calibration - The calibration of the instruments is performed using certified gas standards composed of a known concentration of methane in zero grade nitrogen. These gas standards are prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes an flame ionization detector. The minimum detection limit of the analyzer is 0.1 ppm. Full-scale ranges are available in 100 ppm,

1000 ppm, and 10,000 ppm settings according to the expected concentrations in the flue gas steam. The total organic hydrocarbon concentrations encountered during the testing project enabled the 1000 ppm scale to be used.

As previously mentioned in the carbon monoxide procedure, a low level concentration is employed in conjunction with the high and mid range standards.

2. Sampling - Three test runs were conducted to determine the concentration levels of total organic compounds in the gas stream. Each test run was one hour in duration.

F. Polynuclear Aromatic Hydrocarbons - Method SW846 8270 "Semivolatile Organic Compounds by Gas Chromatography/Mass Spectrometry (GC/MS): Capillary Column Technique

1. Preparation - All glassware utilized in each sampling train was thoroughly cleaned with hot soapy water and dried prior to each test series. All residue *silicon grease* was removed from glassware upstream of the absorbent module. A glass fiber filter was used that has been properly labeled.

The absorbent traps was packed by the analytical laboratory that conducted the final analysis. The impinger system was assembled using 100 ml of D.I. water in impingers 1 and 2. The third impinger was initially empty and the fourth impinger contained silica gel.

In assembling the sample train, teflon tape was placed on the ball joints to ensure adequate sealing upstream of the absorbent module. All connections downstream of the module were sealed with silicon grease.

A glass probe liner and nozzle system was utilized for the collection train. The probe housed a set of calibrated S-type pitot tubes and a calibrated thermocouple for monitoring stack temperature.

2. Sampling - The probe and sample box was heated to an approximate temperature of 250°F. These temperatures were monitored throughout the testing. The probe was connected to the heated filter system with connecting glassware. This filter system was connected to the condenser by a teflon line. The condenser and absorbent module are directly connected via ground glass ball and socket.

An ice bath was prepared to submerge the impinger system into. The temperature of the last impinger was monitored throughout the testing to ensure adequate condensation of the water vapor in the flue gases.

The condenser cooling fluid was recirculated through the system by a peristaltic pump. This pump was started prior to the start up of the sampling system to ensure that the temperature of the absorbent material in the module does not exceed its thermal decomposition temperature. The temperature of gas entering the module was monitored to ensure that the temperature did not exceed the recommended limitation for efficient capture.

A leak check was performed prior to each test run. The entire sample train system was subjected to a vacuum that did not exceed 0.02 cfm leakage rate. The vacuum that was established during the pre-test leak check was not exceeded during the test period.

Three sample runs were conducted to constitute a complete test. The sample time was a minimum of one hour. When a test run was completed, a post-test leak check was conducted prior to any dismantling of the sampling train. Once this had been successfully achieved, the sample train was dismantled for sample recovery.

3. Sample Analysis - Method 8270 is used to determine the concentration of semivolatile organic compounds in extracts prepared from all types of solid waste matrices. Each compound present in the sample is separated by gas chromatography and quantified by mass spectrometry. The detection limitation of this type of sample has been determined to be 1.0 microgram.

If the samples are separated for further analysis, the detection limit will be 2.0 micrograms.

G. EPA Draft Method 202, "Determination of Filterable and Condensable Particulate Matter":

The testing procedures were conducted according to US EPA Reference Method 5 for particulate matter determination. This testing procedure was covered in a previous section. The filterable portion of the particulate matter was determined via this procedure. The condensable fraction of the sample was determined by analyzing the back half impinger catch with a methylene chloride extraction.

This extraction procedure will yield fractions of inorganic and organic condensable matter. The concentrations and emission values of both filterable particulate and condensable particulate matter have been summarized in the test results section.

H. EPA Draft Method 0011, "Determination of Formaldehyde":

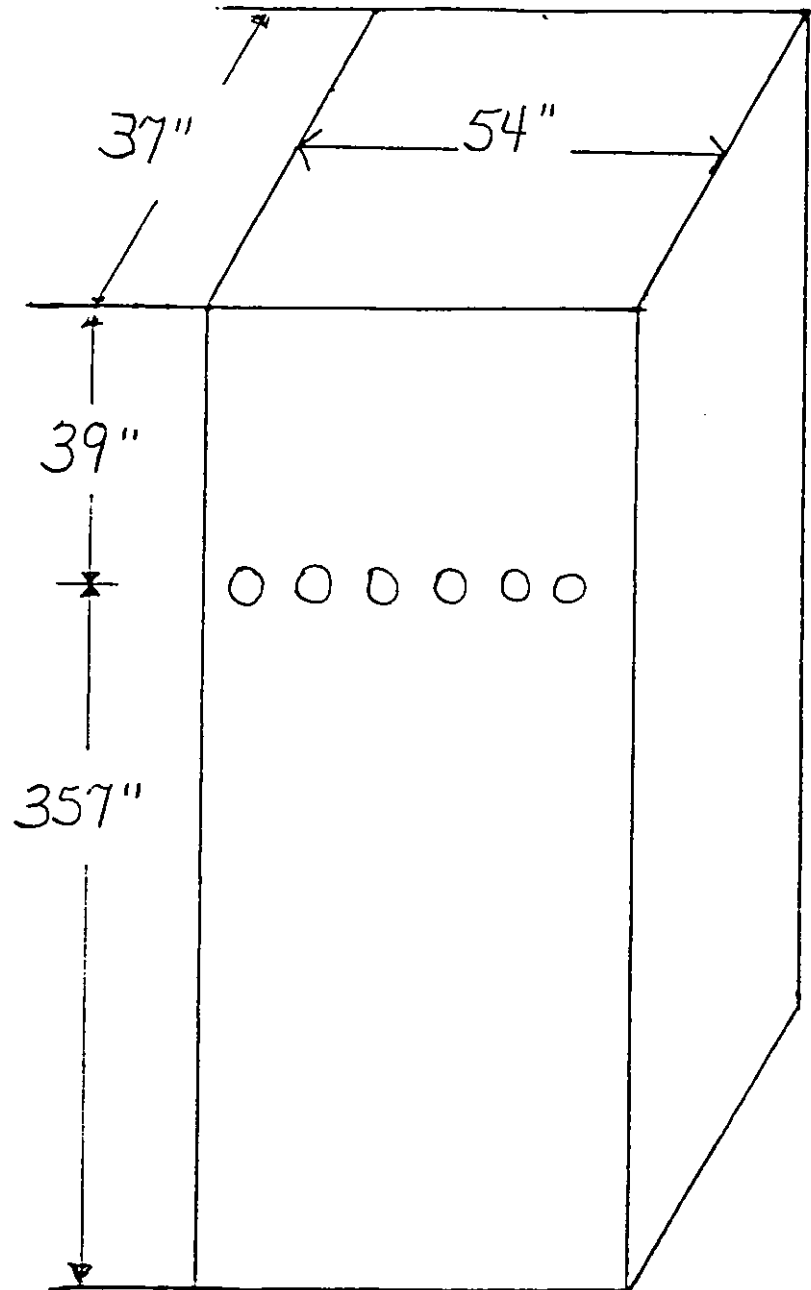
This sampling procedure is similar to the operational procedures found in Reference Method 5. Described in this section are the differences set forth from Method 5 to ensure that the integrity of the formaldehyde sample is maintained.

Prior to any sampling, all glassware was rinsed with methylene chloride to remove any contamination initially on the glassware such as stopcock grease. This includes the rinsing of the glass probe liner material required for the collection of the sample.

In collecting the sample, a minimum of 45 cubic feet must be pulled isokinetically such that the extracted sample is transferred through the DNPH absorption solution. All samples were placed into glass amber sample containers to avoid the alteration of the sample by sunlight.

The analysis of the formaldehyde samples were conducted according to the procedures outlined in Method 8315. This analysis procedure provides guidance in the evaluation of formaldehyde samples by High Performance Liquid Chromatography (HPLC).

Sampling Site: The emissions test was conducted after a baghouse on a rectangular stack measuring 37.0" x 54.0" with an equivalent diameter of 43.9". Six sampling ports were placed 39" down (0.9 diameters upstream) from the top of the stack and 357" up (8.1 diameters downstream) from the last flow disturbance. The ports were evenly spaced on 9.0" centers. The two outside ports are 4.5" from the side walls of the stack. The gaseous samples were taken from an additional sample port located 50" below the original sample ports and located in the center of the stack.



IV. THE SOURCE

Lehman Roberts employs an Standard Havens drum mix asphalt plant which is used to manufacture hot mix asphalt for road pavement. The process consists of blending prescribed portions of cold feed materials (sand, gravel, screenings, chips, etc.) uniformly and adding sufficient hot asphalt oil to bind the mixture together. After the hot asphalt mix is manufactured at the plant, it is transported to the location where it is to be applied. The hot asphalt mix is spread evenly over the surface with a paver then compacted with a heavy roller to produce the final product.

The following is a general description of the plant's manufacturing process: The cold feed materials (aggregate) are dumped into separate bins which in turn feed a common continuous conveyor. The aggregate is dispensed from the bins in accordance with the desired formulation onto the cold feed system conveyor, to an inclined weigh conveyor, then to a rotating drum for continuous mixing and drying at approximately 300°F. When recycled asphalt mix is used, it is added halfway down the drum through a separate conveyor. The required amount of hot asphalt oil is then injected onto and mixed into the dried aggregate. The now newly formed hot asphalt mix is pulled to the top of a storage silo by a conveyor. The hot asphalt mix is then discharged from the storage silo through a slide gate into waiting dump trucks which transports the material to a final destination for spreading. The rated capacity of the plant will vary with each aggregate mix and moisture content with a 5% surface moisture removal.

The drum mixer uses a burner fired with fuel to heat air to dry the aggregate, and the motion of the rotating drum to blend the aggregate. The air is drawn into the system via an exhaust fan. After passing through the gas burner and the mixing drum, the air passes through a baghouse. The exhaust gasses are drawn through the baghouse and discharged to the atmosphere through the stack. The design pressure drop across the tube sheet is 2-6 inches of water. The particulate matter, which is removed by the baghouse, is reinjected into the drum mixer.

Condensable

Run # 1

Lehman - Roberts

09-04-91

09:48:12

Plant Status Report

	Rate	Units	Total	Units
Production	394	Tons Per Hour	737	Tons
Aggregate	319	Tons Per Hour	625.9	Tons
Total A.C.	20.9	Tons Per Hour		
Virgin A.C.	18.7	Tons Per Hour	30.68	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	54	Tons Per Hour	81.1	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix	Temperature	304 Deg.	Sling. Position	19 %
A.C.	Temperature	312 Deg.	Burner Position	69 %
			Damper Position	78 %
Stack	Temperature	278 Deg.		
Instant Actual A.C.	5.30 %		B/H Pulse Time	15 Seconds
Average Actual A.C.	5.26 %		Negative Press	0.15 Inches
			B/H Diff. Press	4.2 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-04-91

09:58:10

Plant Status Report

	Rate	Units	Total	Units
Production	391	Tons Per Hour	806	Tons
Aggregate	311	Tons Per Hour	680.2	Tons
Total A.C.	20.9	Tons Per Hour		
Virgin A.C.	18.5	Tons Per Hour	33.81	Tons
R.A.P. A.C.	2.4	Tons Per Hour		
R.A.P.	59	Tons Per Hour	93.7	Tons
Additive	0	Lbs Per Hour		
Agg. Composite Moisture				4.6 %
Mix Temperature	313	Deg.	Sling. Position	19 %
A.C. Temperature	313	Deg.	Burner Position	68 %
			Damper Position	77 %
Stack Temperature	283	Deg.	B/H Pulse Time	15 Seconds
Instant Actual A.C.	5.35	%	Negative Press	0.15 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	4.3 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C. On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C. Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %			
Feeder # 4	0.0	Mix %	13.7	Moist %			
Feeder # 5	0.0	Mix %	2.7	Moist %			
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set	320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %			
R.A.P.	14.2	Mix %	7.5	Moist %	4.0	A.C. %	
A.C.	5.3	Mix %					
Total		100.0 %	Additive		0.00	Mix %	

Lehman - Roberts

09-04-91

10:08:12

Plant Status Report

	Rate	Units	Total	Units
Production	396	Tons Per Hour	877	Tons
Aggregate	318	Tons Per Hour	733.7	Tons
Total A.C.	21.4	Tons Per Hour		
Virgin A.C.	19.1	Tons Per Hour	36.96	Tons
R.A.P. A.C.	2.3	Tons Per Hour		
R.A.P.	57	Tons Per Hour	106.7	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix	Temperature	301 Deg.	Sling. Position	19 %
A.C.	Temperature	313 Deg.	Burner Position	73 %
			Damper Position	82 %
Stack	Temperature	285 Deg.	B/H Pulse Time	15 Seconds
Instant Actual A.C.	5.40 %		Negative Press	0.14 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	4.5 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			
Total 100.0 %		Additive 0.00 Mix %		

Plant Status Report

	Rate	Units	Total	Units
Production	399	Tons Per Hour	946	Tons
Aggregate	323	Tons Per Hour	787.0	Tons
Total A.C.	21.1	Tons Per Hour		
Virgin A.C.	18.9	Tons Per Hour	40.09	Tons
R.A.P. A.C.	2.3	Tons Per Hour		
R.A.P.	55	Tons Per Hour	119.5	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix	Temperature	303 Deg.	Sling. Position	19 %
A.C.	Temperature	314 Deg.	Burner Position	78 %
			Damper Position	84 %
Stack	Temperature	287 Deg.	B/H Pulse Time	15 Seconds
Instant Actual A.C.	5.28 %		Negative Press	0.15 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	4.6 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			
Total 100.0 %		Additive 0.00 Mix %		

Name : 307-A
 Description : 307-A LIMESTONE

Feeder # 1	28.9 Mix %	3.4 Moist %	A.C.	On Time	215 Sec
Feeder # 2	36.6 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	0.0 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	30.9 Mix %	2.7 Moist %			
Feeder # 6	0.0 Mix %	2.6 Moist %	Mix Temp Set		300 Deg
Feeder # 7	0.0 Mix %	4.9 Moist %			
R.A.P.	0.0 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	3.6 Mix %				

Total 100.0 % Additive 0.00 Mix %

09-04-91 10:23:18 Change Mix On

09-04-91 10:26:17 Bin #1 High

09-04-91 10:27:57 Asphalt Deviation

09-04-91 Lehman - Roberts 10:28:11
 Plant Status Report

	Rate	Units	Total	Units
Production	410	Tons Per Hour	1020	Tons
Aggregate	396	Tons Per Hour	844.8	Tons
Total A.C.	14.1	Tons Per Hour		
Virgin A.C.	14.1	Tons Per Hour	43.06	Tons
R.A.P. A.C.	0.0	Tons Per Hour		
R.A.P.	0	Tons Per Hour	132.0	Tons

Hgg. Composite Moisture 2.0 %

Mix Temperature 272 Deg. Sling Position 19 %
 A.C. Temperature 314 Deg. Burner Position 27 %
 Damper Position 54 %
 Stack Temperature 292 Deg. B/H Pulse Time 15 Seconds
 Instant Actual A.C. 3.43 % Negative Press 0.19 Inches
 Average Actual A.C. 5.00 % B/H Diff. Press 3.3 Inches

Running Mix # 4
 Name : 307-A
 Description : 307-A LIMESTONE

Feeder # 1	28.9 Mix %	3.4 Moist %	A.C.	On Time	215 Sec
Feeder # 2	36.6 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	0.0 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	30.9 Mix %	2.7 Moist %			
Feeder # 6	0.0 Mix %	2.6 Moist %	Mix Temp Set		300 Deg
Feeder # 7	0.0 Mix %	4.9 Moist %			
R.A.P.	0.0 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	3.6 Mix %				

Total 100.0 % Additive 0.00 Mix %

09-04-91 10:28:16 Change Mix Complete

09-04-91 10:28:35 Bin #1 High

Lehman - Roberts

09-04-91

10:38:10

Plant Status Report

	Rate	Units	Total	Units
Production	397	Tons Per Hour	1087	Tons
Aggregate	383	Tons Per Hour	909.2	Tons
Total A.C.	14.2	Tons Per Hour		
Virgin A.C.	14.2	Tons Per Hour	45.47	Tons

R.A.P. 0 Tons Per Hour 132.0 Tons

Additive 0 Lbs Per Hour

Agg. Composite Moisture 2.8 %

Mix	Temperature	310 Deg.	Sling. Position	19 %
A.C.	Temperature	315 Deg.	Burner Position	26 %
			Damper Position	46 %
Stack	Temperature	260 Deg.	B/H Pulse Time	15 Seconds
Instant Actual A.C.	3.57 %	Negative Press	0.16 Inches	
Average Actual A.C.	3.59 %	B/H Diff. Press	1.7 Inches	

Running Mix # 4
 Name : 307-A
 Description : 307-A LIMESTONE

Feeder # 1	28.9 Mix %	3.4 Moist %	A.C.	On Time	215 Sec
Feeder # 2	36.6 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	0.0 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	30.9 Mix %	2.7 Moist %			
Feeder # 6	0.0 Mix %	2.6 Moist %	Mix Temp Set	300 Deg	
Feeder # 7	0.0 Mix %	4.9 Moist %			

R.A.P. 0.0 Mix % 7.5 Moist % 4.0 A.C. %
 A.C. 3.6 Mix %

 Total 100.0 % Additive 0.00 Mix %

Lehman - Roberts

09-04-91

10:38:42

Change to New Mix

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg	
Feeder # 7	28.4 Mix %	4.9 Moist %			

R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %

Total 100.0 %

Additive 0.00 Mix %

09-04-91 10:38:44 Change Mix On

09-04-91 10:43:06 RAP Crusher High Amperage

09-04-91 10:43:18 Recycle Deviation

09-04-91 10:43:32 Asphalt Deviation

09-04-91 10:43:40 Change Mix Complete

09-04-91 10:43:51 Asphalt Deviation

Lehman - Roberts

09-04-91

10:48:10

Plant Status Report

	Rate	Units	Total	Units
* Production	378	Tons Per Hour	1149	Tons
* Aggregate	309	Tons Per Hour	964.3	Tons
* Total A.C.	20.2	Tons Per Hour		
* Virgin A.C.	18.2	Tons Per Hour	48.33	Tons
* P.O.D. A.C.	2.0	Tons Per Hour		

```

*
* Additive      0      Lbs Per Hour
*
*                               Agg. Composite Moisture  4.6%
*
* Mix      Temperature  306 Deg.      Sling. Position  19 %
* A.C.     Temperature  316 Deg.      Burner Position  68 %
*
*                               Damper Position  68 %
*
* Stack     Temperature  269 Deg.
*
*                               B/H Pulse Time  15      Seconds
* Instant Actual A.C.  5.34 %      Negative Press  0.14 Inches
* Average Actual A.C.  4.64 %      B/H Diff. Press  3.2 Inches
*
*****

```

```

*
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*
-----

```

```

* Feeder # 1  9.5 Mix %   3.4 Moist %   A.C.   On Time  245 Sec
* Feeder # 2  0.0 Mix %   2.5 Moist %   A.C.   Off Time  200 Sec
* Feeder # 3  6.6 Mix %  15.7 Moist %
* Feeder # 4  0.0 Mix %  13.7 Moist %
* Feeder # 5  0.0 Mix %   2.7 Moist %
* Feeder # 6  36.0 Mix %   2.6 Moist %   Mix Temp Set  320 Deg
* Feeder # 7  28.4 Mix %   4.9 Moist %
*
* R.A.P.      14.2 Mix %   7.5 Moist %   4.0 A.C. %
*
* A.C.        5.3 Mix %
*
*
* -----
* Total      100.0 %
*
*                               Additive  0.00 Mix %
*
*****

```

```

*****
*
*                               Lehman - Roberts
*                               09-04-91                               10:58:11
*                               Plant Status Report
*
*****

```

```

*                               Rate   Units           Total   Units
* -----
* Production      406   Tons Per Hour   1219   Tons
* Aggregate       323   Tons Per Hour   1018.0 Tons
* Total A.C.      21.5 Tons Per Hour
* Virgin A.C.     19.0 Tons Per Hour   51.46 Tons
*
* R.A.P. A.C.     2.5 Tons Per Hour
*
* R.A.P.          61   Tons Per Hour   149.8 Tons
*
* Additive        0   Lbs Per Hour
*
*                               Agg. Composite Moisture  4.6%
*
*****

```


H.C. Temperature 316 Deg. Burner Position 82 %
 Damper Position 80 %
 Stack Temperature 282 Deg.
 B/H Pulse Time 15 Seconds
 Instant Actual A.C. 5.29 % Negative Press 0.16 Inches
 Average Actual A.C. 5.29 % B/H Diff. Press 4.2 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Sec
1	9.5	3.4	A.C.	245		245
2	0.0	2.5	A.C.		200	200
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total 100.0 %		Additive 0.00 Mix %				

Lehman - Roberts
 09-04-91
 Plant Status Report

10:58:36

	Rate	Units	Total	Units
Production	411	Tons Per Hour	1221	Tons
Aggregate	328	Tons Per Hour	1020.3	Tons
Total A.C.	21.7	Tons Per Hour		
Virgin A.C.	19.2	Tons Per Hour	51.59	Tons
R.A.P. A.C.	2.5	Tons Per Hour		
R.A.P.	61	Tons Per Hour	150.3	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %

Mix Temperature 290 Deg. Sling. Position 19 %
 A.C. Temperature 316 Deg. Burner Position 84 %
 Damper Position 80 %
 Stack Temperature 283 Deg.
 B/H Pulse Time 15 Seconds
 Instant Actual A.C. 5.25 % Negative Press 0.17 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				

Total 100.0 % Additive 0.00 Mix %

Condensables

Is X

JM

Condensables

09-04-91 11:10:55 Feeder MAX TPH Calibration Error

09-04-91 11:28:07 Feeder MAX TPH Calibration Error

09-04-91 11:34:29 Bin #1 Low

09-04-91 11:38:40 Feeder MAX TPH Calibration Error

09-04-91 11:48:34 Bin #4 High

09-04-91 11:58:31 Feeder MAX TPH Calibration Error

* Lehman - Roberts *

* 09-04-91 12:01:12 *

* Plant Status Report *

	Rate	Units	Total	Units
* Production	402	Tons Per Hour	1660	Tons
* Aggregate	324	Tons Per Hour	1358.7	Tons
* Total A.C.	21.1	Tons Per Hour		
* Virgin A.C.	18.8	Tons Per Hour	71.38	Tons
* R.A.P. A.C.	2.3	Tons Per Hour		
* R.A.P.	57	Tons Per Hour	229.9	Tons
* Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %

```

* Mix Temperature 318 Deg. Sling Position 19 %
* A.C. Temperature 319 Deg. Burner Position 81 %
* Damper Position 85 %
* Stack Temperature 287 Deg.
* B/H Pulse Time 15 Seconds
* Instant Actual A.C. 5.26 % Negative Press 0.19 Inches
* Average Actual A.C. 5.27 % B/H Diff. Press 4.8 Inches

```

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Temp / Sec
1	9.5	3.4	A.C.	245		Sec
2	0.0	2.5	A.C.	200		Sec
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total		100.0 %	Additive	0.00		Mix %

09-04-91 12:05:53 Feeder MAX TPH Calibration Error

```

*****
* Lehman - Roberts
* 09-04-91 12:10:13
* Plant Status Report

```

	Rate	Units	Total	Units
Production	403	Tons Per Hour	1723	Tons
Aggregate	329	Tons Per Hour	1407.9	Tons
Total A.C.	21.2	Tons Per Hour		
Virgin A.C.	19.0	Tons Per Hour	74.22	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	53	Tons Per Hour	241.5	Tons
Additive	0	Lbs Per Hour		
Agg. Composite Moisture 4.6 %				

```

* H.C. Temperature 320 Deg. Burner Position 80 %
* Stack Temperature 281 Deg. Damper Position 85 %
* Instant Actual A.C. 5.26 % B/H Pulse Time 15 Seconds
* Average Actual A.C. 5.28 % Negative Press 0.19 Inches
* B/H Diff. Press 4.6 Inches

```

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*-----*
* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
* A.C. 5.3 Mix %
*-----*
* Total 100.0 % Additive 0.00 Mix %
*-----*

```

09-04-91 12:19:46 Feeder MAX TPH Calibration Error

```

*****
* Lehman - Roberts
* 09-04-91 12:20:12
* Plant Status Report
*-----*
* Rate Units Total Units
*-----*
* Production 394 Tons Per Hour 1792 Tons
* Aggregate 317 Tons Per Hour 1461.4 Tons
* Total A.C. 21.0 Tons Per Hour
* Virgin A.C. 18.7 Tons Per Hour 77.37 Tons
* R.A.P. A.C. 2.2 Tons Per Hour
* R.A.P. 56 Tons Per Hour 254.4 Tons
* Additive 0 Lbs Per Hour
* Agg. Composite Moisture 4.6 %

```

* Damper Position 88 % *
 * Stack Temperature 292 Deg *
 * B/H Pulse Time 15 Seconds *
 * Instant Actual A.C. 5.31 % Negative Press 0.17 Inches *
 * Average Actual A.C. 5.29 % B/H Diff. Press 4.9 Inches *
 * ***** *

* Running Mix # 51 *
 * Name : 411-E *
 * Description : 411-E/W RAP AC IN RAP 3.5% *
 * ----- *

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				

Total	100.0 %		Additive	0.00 Mix %	

* ***** *

* Lehman - Roberts *
 * 09-04-91 12:30:13 *
 * Plant Status Report *
 * ***** *

	Rate	Units	Total	Units
Production	401	Tons Per Hour	1862	Tons
Aggregate	322	Tons Per Hour	1514.8	Tons
Total A.C.	21.1	Tons Per Hour		
Virgin A.C.	18.7	Tons Per Hour	80.51	Tons
R.A.P. A.C.	2.4	Tons Per Hour		
R.A.P.	58	Tons Per Hour	267.5	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	307	Deg.	Sling. Position	19 %
A.C. Temperature	321	Deg.	Burner Position	71 %
			Damper Position	89 %
Stack Temperature	286	Deg.		
			B/H Pulse Time	15 Seconds
Instant Actual A.C.	5.26 %		Negative Press	0.19 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	5.0 Inches

* ***** *

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			

R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %

A.C. 5.3 Mix %

Total 100.0 %

Additive 0.00 Mix %

09-04-91 12:34:07 Feeder MAX TPH Calibration Error

Lehman - Roberts

09-04-91

12:40:12

Plant Status Report

	Rate	Units	Total	Units
Production	398	Tons Per Hour	1932	Tons
Aggregate	323	Tons Per Hour	1568.9	Tons
Total A.C.	21.2	Tons Per Hour		
Virgin A.C.	19.0	Tons Per Hour	83.64	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	54	Tons Per Hour	280.4	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix Temperature	309	Deg.	Sling. Position	19 %
A.C. Temperature	321	Deg.	Burner Position	70 %
			Damper Position	80 %
Stack Temperature	286	Deg.		
			B/H Pulse Time	15 Seconds
Instant Actual A.C.	5.31	%	Negative Press	0.17 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	4.6 Inches

```

* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*-----*
* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
*-----*
* Total 100.0 % Additive 0.00 Mix %
*
*****

```

09-04-91 12:49:49 Bin #5 High

```

*****
*
* Lshman - Roberts
* 09-04-91 12:50:12
* Plant Status Report
*
*****
* Rate Units Total Units
*-----*
* Production 398 Tons Per Hour 2001 Tons
* Aggregate 321 Tons Per Hour 1622.2 Tons
* Total A.C. 21.1 Tons Per Hour
* Virgin A.C. 18.8 Tons Per Hour 86.78 Tons
*
* R.A.P. A.C. 2.3 Tons Per Hour
*
* R.A.P. 56 Tons Per Hour 293.3 Tons
*
* Additive 0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 299 Deg. Sling. Position 19 %
* A.C. Temperature 321 Deg. Burner Position 71 %
* Damper Position 76 %
*
* Stack Temperature 275 Deg.
* B/H Pulse Time 15 Seconds
* Instant Actual A.C. 5.30 % Negative Press 0.17 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 4.5 Inches
*****

```



```

* Feeder # 1  9.5 Mix %   3.4 Moist %   A.C.   On Time 245 Sec
* Feeder # 2  0.0 Mix %   2.5 Moist %   A.C.   Off Time 200 Sec
* Feeder # 3  6.6 Mix %   15.7 Moist %
* Feeder # 4  0.0 Mix %   13.7 Moist %
* Feeder # 5  0.0 Mix %   2.7 Moist %
* Feeder # 6  36.0 Mix %   2.6 Moist %   Mix Temp Set      320 Deg
* Feeder # 7  28.4 Mix %   4.9 Moist %
*
* R.A.P.      14.2 Mix %   7.5 Moist %   4.0 A.C. %
*
* A.C.        5.3 Mix %

```

```

* -----
* Total      100.0 %           Additive    0.00 Mix %

```

Lehman - Roberts

09-04-91

12:50:30

Plant Status Report

	Rate	Units	Total	Units
Production	417	Tons Per Hour	2023	Tons
Aggregate	341	Tons Per Hour	1623.6	Tons
Total A.C.	21.2	Tons Per Hour		
Virgin A.C.	19.1	Tons Per Hour	86.87	Tons
R.A.P. A.C.	2.3	Tons Per Hour		
R.A.P.	55	Tons Per Hour	293.7	Tons
Additive	0	Lbs Per Hour		

Agg. Composite Moisture 4.6 %

```

* Mix Temperature 301 Deg.   Sling. Position 19 %
* A.C. Temperature 321 Deg.   Burner Position 71 %
*                               Damper Position 76 %
* Stack Temperature 274 Deg.
*                               B/H Pulse Time 15 Seconds
* Instant Actual A.C. 5.09 %   Negative Press 0.17 Inches
* Average Actual A.C. 5.23 %   B/H Diff. Press 4.4 Inches

```

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

```

* Feeder # 1  9.5 Mix %   3.4 Moist %   A.C.   On Time 245 Sec
* Feeder # 2  0.0 Mix %   2.5 Moist %   A.C.   Off Time 200 Sec
* Feeder # 3  6.6 Mix %   15.7 Moist %
* Feeder # 4  0.0 Mix %   13.7 Moist %

```

```

* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg *
* Feeder # 7 28.4 Mix % 4.9 Moist % *
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. % *
* A.C. 5.3 Mix % *
*
* ----- *
* Total 100.0 % Additive 0.00 Mix % *
*
*

```

09-04-91 12:59:32 Feeder MAX TPH Calibration Error

09-04-91 13:09:03 Feeder MAX TPH Calibration Error

3rd

Condensates

09-04-91 13:17:16 Bin #4 High

09-04-91 13:25:35 Bin #5 High

09-04-91 13:26:19 Bin Top Conveyor Right Overtravel

Lehman - Roberts

09-04-91

13:35:09

Plant Status Report

	Rate	Units	Total	Units
* Production	401	Tons Per Hour	2315	Tons
* Aggregate	323	Tons Per Hour	1864.1	Tons
* Total A.C.	21.0	Tons Per Hour		
* Virgin A.C.	18.7	Tons Per Hour	100.90	Tons
* R.A.P. A.C.	2.4	Tons Per Hour		
* R.A.P.	57	Tons Per Hour	351.3	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix Temperature	315	Deg.	Sling. Position	19 %
* A.C. Temperature	322	Deg.	Burner Position	84 %
			Damper Position	88 %
* Stack Temperature	291	Deg.	B/H Pulse Time	10 Seconds
* Instant Actual A.C.	5.22	%	Negative Press	0.19 Inches
* Average Actual A.C.	5.31	%	B/H Diff. Press	4.4 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1	9.5	Mix %	3.4	Moist %	A.C.	On Time	245	Sec
* Feeder # 2	0.0	Mix %	2.5	Moist %	A.C.	Off Time	200	Sec
* Feeder # 3	6.6	Mix %	15.7	Moist %				
* Feeder # 4	0.0	Mix %	13.7	Moist %				

```

* Feeder # 6 30.0 Mix % 4.0 Moist %
* Feeder # 7 28.4 Mix % 4.9 Moist %
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
* A.C. 5.3-Mix %
*
* -----
* Total 100.0 % Additive 0.00 Mix %
*
*****

```

09-04-91 13:35:13 Feeder MAX TPH Calibration Error

09-04-91 13:47:15 Bin #3 High

09-04-91 13:47:43 Bin Top Conveyor Right Overtravel

09-04-91 13:54:06 Feeder MAX TPH Calibration Error

```

*****
*
* Lehman - Roberts
* 09-04-91 13:54:13
* Plant Status Report
*
*****

```

	Rate	Units	Total	Units
Production	399	Tons Per Hour	2449	Tons
Aggregate	321	Tons Per Hour	1966.8	Tons
Total A.C.	21.3	Tons Per Hour		
Virgin A.C.	19.0	Tons Per Hour	106.90	Tons
R.A.P. A.C.	2.3	Tons Per Hour		
R.A.P.	57	Tons Per Hour	376.0	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %

Temperature 291 Deg. Damper Position 90 %
 Stack Temperature 291 Deg. B/H Pulse Time 10 Seconds
 Instant Actual A.C. 5.33 % Negative Press 0.20 Inches
 Average Actual A.C. 5.29 % B/H Diff. Press 4.4 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Sec
1	9.5	3.4	A.C.	245		245
2	0.0	2.5	A.C.		200	200
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total	100.0 %		Additive	0.00	Mix %	

 Lehman - Roberts
 09-04-91 14:04:14
 Plant Status Report

	Rate	Units	Total	Units
Production	399	Tons Per Hour	2518	Tons
Aggregate	325	Tons Per Hour	2020.4	Tons
Total A.C.	21.2	Tons Per Hour		
Virgin A.C.	19.0	Tons Per Hour	110.06	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	53	Tons Per Hour	388.7	Tons
Additive	0	Lbs Per Hour		

Agg. Composite Moisture 4.6 %

Mix Temperature 314 Deg. Sling. Position 19 %
 A.C. Temperature 323 Deg. Burner Position 78 %
 Damper Position 90 %
 Stack Temperature 290 Deg.
 B/H Pulse Time 10 Seconds
 Instant Actual A.C. 5.31 % Negative Press 0.20 Inches
 Average Actual A.C. 5.29 % B/H Diff. Press 4.4 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			

R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %
A.C.	5.3 Mix %		

Total 100.0 % Additive 0.00 Mix %

09-04-91 Lehman - Roberts 14:14:13
 Plant Status Report

	Rate	Units	Total	Units
Production	401	Tons Per Hour	2539	Tons
Aggregate	324	Tons Per Hour	2074.2	Tons
Total A.C.	21.3	Tons Per Hour		
Virgin A.C.	19.0	Tons Per Hour	113.21	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	56	Tons Per Hour	401.7	Tons

Additive 0 Lbs Per Hour
 Agg. Composite Moisture 4.6 %

Mix Temperature	321 Deg.	Sling. Position	19 %
A.C. Temperature	323 Deg.	Burner Position	73 %
		Damper Position	90 %
Stack Temperature	294 Deg.	B/H Pulse Time	10 Seconds
Instant Actual A.C.	5.30 %	Negative Press	0.19 Inches
Average Actual A.C.	5.29 %	B/H Diff. Press	4.5 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec

```

* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
*
*
* Total 100.0 % Additive 0.00 Mix %
*
*
*

```

09-04-91 14:16:23 Feeder MAX TPH Calibration Error

09-04-91 14:23:13 Bin #5 High

```

*****
*
* Lehman - Roberts
* 09-04-91 14:24:14
* Plant Status Report
*

```

```

*****
*
* Rate Units Total Units
* -----
* Production 402 Tons Per Hour 2659 Tons
* Aggregate 326 Tons Per Hour 2128.6 Tons
* Total A.C. 21.1 Tons Per Hour
* Virgin A.C. 18.9 Tons Per Hour 116.38 Tons
*
* R.A.P. A.C. 2.3 Tons Per Hour
*
* R.A.P. 55 Tons Per Hour 414.6 Tons
*
* Additive 0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 319 Deg. Sling. Position 19 %
* A.C. Temperature 324 Deg. Burner Position 66 %
* Damper Position 85 %
*
* Stack Temperature 292 Deg.
*
* B/H Pulse Time 10 Seconds
* Instant Actual A.C. 5.23 % Negative Press 0.17 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 4.3 Inches
*
*****

```

Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
* Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
* Feeder # 3	6.6 Mix %	15.7 Moist %			
* Feeder # 4	0.0 Mix %	13.7 Moist %			
* Feeder # 5	0.0 Mix %	2.7 Moist %			
* Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
* Feeder # 7	28.4 Mix %	4.9 Moist %			
* R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
* A.C.	5.3 Mix %				

* Total	100.0 %		Additive	0.00 Mix %	

09-04-91 14:28:37 Feeder MAX TPH Calibration Error

Lehman - Roberts

09-04-91

14:34:14

Plant Status Report

	Rate	Units	Total	Units
* Production	401	Tons Per Hour	2728	Tons
* Aggregate	326	Tons Per Hour	2182.2	Tons
* Total A.C.	21.2	Tons Per Hour		
* Virgin A.C.	19.0	Tons Per Hour	119.53	Tons
* R.A.P. A.C.	2.2	Tons Per Hour		
* R.A.P.	54	Tons Per Hour	427.4	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix Temperature	308	Deg.	Sling Position	19 %
* A.C. Temperature	323	Deg.	Burner Position	70 %
			Damper Position	80 %
* Stack Temperature	288	Deg.	B/H Pulse Time	10 Seconds
* Instant Actual A.C.	5.28	%	Negative Press	0.19 Inches
* Average Actual A.C.	5.29	%	B/H Diff. Press	4.3 Inches


```

*-----*
* Feeder # 1  9.5 Mix %    3.4 Moist %    A.C.    On Time 245 Sec
* Feeder # 2  0.0 Mix %    2.5 Moist %    A.C.    Off Time 200 Sec
* Feeder # 3  6.6 Mix %    15.7 Moist %
* Feeder # 4  0.0 Mix %    13.7 Moist %
* Feeder # 5  0.0 Mix %    2.7 Moist %
* Feeder # 6  36.0 Mix %    2.6 Moist %    Mix Temp Set    320 Deg
* Feeder # 7  28.4 Mix %    4.9 Moist %
*
* R.A.P.      14.2 Mix %    7.5 Moist %    4.0 A.C. %
*
* A.C.        5.3 Mix %
*
*-----*
* Total      100.0 %
* Additive   0.00 Mix %
*-----*

```

```

*****
*
* Lehman - Roberts
* 09-04-91 14:38:05
* Plant Status Report
*
*****

```

```

*****
* Rate Units Total Units
*-----*
* Production 400 Tons Per Hour 2755 Tons
* Aggregate 325 Tons Per Hour 2203.1 Tons
* Total A.C. 21.1 Tons Per Hour
* Virgin A.C. 18.9 Tons Per Hour 120.75 Tons
*
* R.A.P. A.C. 2.2 Tons Per Hour
*
* R.A.P. 54 Tons Per Hour 432.2 Tons
*
* Additive 0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 313 Deg. Sling. Position 19 %
* A.C. Temperature 324 Deg. Burner Position 69 %
* Damper Position 80 %
*
* Stack Temperature 285 Deg.
*
* B/H Pulse Time 10 Seconds
* Instant Actual A.C. 5.27 % Negative Press 0.18 Inches
* Average Actual A.C. 5.30 % B/H Diff. Press 4.2 Inches
*-----*

```

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*-----*

```

```

* Feeder # 1  9.5 Mix %    3.4 Moist %    A.C.    On Time 245 Sec
* Feeder # 2  0.0 Mix %    2.5 Moist %    A.C.    Off Time 200 Sec
* Feeder # 3  6.6 Mix %    15.7 Moist %
* Feeder # 4  0.0 Mix %    13.7 Moist %

```

```

* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
* A.C. 5.3 Mix %
*
* -----
* Total 100.0 % Additive 0.00 Mix %
*
*****

```

09-04-91 14:38:26 Feeder MAX TPH Calibration Error

09-04-91 14:38:34 Main Flame Failure

09-04-91 14:38:36 Asphalt Valve Recirculate

09-04-91 14:38:38 System Stop

Gaseous & PAH's
Run 1

09-03-91 09:39:46 Asphalt Deviation

09-03-91 09:46:54 Feeder MAX TPH Calibration Error

*
* Lehman - Roberts *
* 09-03-91 11:26:11 *
* Plant Status Report *

	Rate	Units	Total	Units
Production	348	Tons Per Hour	1158	Tons
Aggregate	283	Tons Per Hour	895.6	Tons
Total A.C.	18.4	Tons Per Hour		
Virgin A.C.	16.5	Tons Per Hour	52.47	Tons
R.A.P. A.C.	1.9	Tons Per Hour		
R.A.P.	47	Tons Per Hour	210.5	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix Temperature	307	Deg.	Sling. Position	3 %
A.C. Temperature	299	Deg.	Burner Position	45 %
Stack Temperature	246	Deg.	Damper Position	61 %
Instant Actual A.C.	5.27	%	B/H Pulse Time	25 Seconds
Average Actual A.C.	5.31	%	Negative Press	0.10 Inches
			B/H Diff. Press	3.3 Inches

*
* Running Mix # 51 *
* Name : 411-E *
* Description : 411-E/W RAP AC IN RAP 3.5% *

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C. On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C. Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %			
Feeder # 4	0.0	Mix %	13.7	Moist %			
Feeder # 5	0.0	Mix %	2.7	Moist %			
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set	320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %			
R.A.P.	14.2	Mix %	6.2	Moist %	4.0	A.C. %	

Total 100.0 %

Additive 0.00 Mix %

09-03-91

Lehman - Roberts

11:35:51

Plant Status Report

	Rate	Units	Total	Units
Production	346	Tons Per Hour	1217	Tons
Aggregate	281	Tons Per Hour	941.0	Tons
Total A.C.	18.1	Tons Per Hour		
Virgin A.C.	16.2	Tons Per Hour	55.13	Tons
R.A.P. A.C.	1.9	Tons Per Hour		
R.A.P.	47	Tons Per Hour	220.9	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix	Temperature	308 Deg.	Sling. Position	8 %
A.C.	Temperature	300 Deg.	Burner Position	46 %
			Damper Position	61 %
Stack	Temperature	246 Deg.		
			B/H Pulse Time	30 Seconds
Instant Actual A.C.	5.23 %		Negative Press	0.08 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	3.3 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	6.2 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-03-91

11:45:53

Plant Status Report

	Rate	Units	Total	Units
Production	352	Tons Per Hour	1277	Tons
Aggregate	285	Tons Per Hour	987.8	Tons
Total A.C.	18.7	Tons Per Hour		
Virgin A.C.	16.7	Tons Per Hour	57.88	Tons
R.A.P. A.C.	2.0	Tons Per Hour		
R.A.P.	48	Tons Per Hour	232.2	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	305	Deg.	Sling. Position	11 %
A.C. Temperature	300	Deg.	Burner Position	50 %
Stack Temperature	247	Deg.	Damper Position	61 %
Instant Actual A.C.	5.31	%	B/H Pulse Time	30 Seconds
Average Actual A.C.	5.28	%	Negative Press	0.10 Inches
			B/H Diff. Press	3.6 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C.	On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C.	Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %				
Feeder # 4	0.0	Mix %	13.7	Moist %				
Feeder # 5	0.0	Mix %	2.7	Moist %				
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set		320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %				
R.A.P.	14.2	Mix %	6.2	Moist %	4.0	A.C. %		
A.C.	5.3	Mix %						
Total		100.0 %	Additive		0.00	Mix %		

Plant Status Report

	Rate	Units	Total	Units
Production	354	Tons Per Hour	1337	Tons
Aggregate	284	Tons Per Hour	1034.4	Tons
Total A.C.	18.7	Tons Per Hour		
Virgin A.C.	16.6	Tons Per Hour	60.61	Tons
R.A.P. A.C.	2.1	Tons Per Hour		
R.A.P.	51	Tons Per Hour	243.6	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	291	Deg.	Sling. Position	30 %
A.C. Temperature	300	Deg.	Burner Position	59 %
			Damper Position	64 %
Stack Temperature	247	Deg.	B/H Pulse Time	30 Seconds
Instant Actual A.C.	5.26	%	Negative Press	0.07 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	4.1 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C.	On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C.	Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %				
Feeder # 4	0.0	Mix %	13.7	Moist %				
Feeder # 5	0.0	Mix %	2.7	Moist %				
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set		320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %				
R.A.P.	14.2	Mix %	6.2	Moist %	4.0	A.C. %		
A.C.	5.3	Mix %						
Total		100.0 %			Additive	0.00	Mix %	

```

* Production      355 Tons Per Hour      1400 Tons
* Aggregate      285 Tons Per Hour      1082.0 Tons
* Total A.C.     18.5 Tons Per Hour
* Virgin A.C.    16.4 Tons Per Hour      63.37 Tons
*
* R.A.P. A.C.    2.1 Tons Per Hour
*
* R.A.P.         51 Tons Per Hour      254.9 Tons
*
* Additive       0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 325 Deg.      Sling. Position 42 %
* A.C. Temperature 300 Deg.     Burner Position 51 %
*
* Stack Temperature 268 Deg.     Damper Position 61 %
*
* B/H Pulse Time 30 Seconds
* Instant Actual A.C. 5.23 %      Negative Press 0.08 Inches
* Average Actual A.C. 5.28 %     B/H Diff. Press 4.4 Inches

```

```

*
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
* -----
* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 6.2 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
* Total 100.0 % Additive 0.00 Mix %
*
* *****

```

```

*
* Lehman - Roberts
* 09-03-91 12:15:54
* Plant Status Report
*
* *****

```

```

* Rate Units Total Units
* -----
* Production 353 Tons Per Hour 1461 Tons
* Aggregate 285 Tons Per Hour 1129.0 Tons
* Total A.C. 18.7 Tons Per Hour
* Virgin A.C. 16.6 Tons Per Hour 66.13 Tons
*
* *****

```

```

* R.A.P. 49 Tons Per Hour 266.3 Tons
* Additive 0 Lbs Per Hour
* Agg. Composite Moisture 4.6 %
* Mix Temperature 306 Deg. Sling. Position 42 %
* A.C. Temperature 300 Deg. Burner Position 53 %
* Damper Position 61 %
* Stack Temperature 258 Deg.
* B/H Pulse Time 30 Seconds
* Instant Actual A.C. 5.25 % Negative Press 0.08 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 3.7 Inches

```

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

```

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
* R.A.P. 14.2 Mix % 6.2 Moist % 4.0 A.C. %
* A.C. 5.3 Mix %
* Total 100.0 % Additive 0.00 Mix %

```

```

*****
* Lehman - Roberts
* 09-03-91 12:25:54
* Plant Status Report

```

```

*****
* Rate Units Total Units
* Production 345 Tons Per Hour 1522 Tons
* Aggregate 279 Tons Per Hour 1175.6 Tons
* Total A.C. 18.2 Tons Per Hour
* Virgin A.C. 16.3 Tons Per Hour 68.87 Tons
* R.A.P. A.C. 1.9 Tons Per Hour
* R.A.P. 48 Tons Per Hour 277.6 Tons
* Additive 0 Lbs Per Hour
* Agg. Composite Moisture 4.6 %

```


* A.C. Temperature 300 Deg. Burner Position 53 % *
 * Damper Position 61 % *
 * Stack Temperature 259 Deg. B/H Pulse Time 30 Seconds *
 * Instant Actual A.C. 5.27 % Negative Press 0.08 Inches *
 * Average Actual A.C. 5.29 % B/H Diff. Press 3.7 Inches *

* Running Mix # 51 *
 * Name : 411-E *
 * Description : 411-E/W RAP AC IN RAP 3.5% *

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Sec
1	9.5	3.4				245
2	0.0	2.5				200
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6		Mix Temp Set		320 Deg
7	28.4	4.9				
R.A.P.	14.2	6.2	4.0 A.C. %			
A.C.	5.3					
Total 100.0 %		Additive 0.00 Mix %				

 * Lehman - Roberts *
 * 09-03-91 12:35:56 *
 * Plant Status Report *

	Rate	Units	Total	Units
Production	351	Tons Per Hour	1582	Tons
Aggregate	285	Tons Per Hour	1223.1	Tons
Total A.C.	18.8	Tons Per Hour		
Virgin A.C.	16.9	Tons Per Hour	71.62	Tons
R.A.P. A.C.	1.9	Tons Per Hour		
R.A.P.	47	Tons Per Hour	288.7	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %

* Mix Temperature 316 Deg. Sling. Position 42 % *
 * A.C. Temperature 300 Deg. Burner Position 48 % *
 * Damper Position 64 % *
 * Stack Temperature 263 Deg. B/H Pulse Time 30 Seconds *
 * Instant Actual A.C. 5.35 % Negative Press 0.10 Inches *

* Running Mix # 51 *

* Name : 411-E *

* Description : 411-E/W RAP AC-IN RAP 3.5% *

* ↑

* Feeder # 1	9.5	Mix %	3.4	Moist %	A.C.	On Time	245	Sec	*
* Feeder # 2	0.0	Mix %	2.5	Moist %	A.C.	Off Time	200	Sec	*
* Feeder # 3	6.6	Mix %	15.7	Moist %					*
* Feeder # 4	0.0	Mix %	13.7	Moist %					*
* Feeder # 5	0.0	Mix %	2.7	Moist %					*
* Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set		320	Deg	*
* Feeder # 7	28.4	Mix %	4.9	Moist %					*
* R.A.P.	14.2	Mix %	6.2	Moist %	4.0	A.C. %			*
* A.C.	5.3	Mix %							*
* Total	100.0	%			Additive	0.00	Mix %		*

* *****

09-03-91 12:37:20 Feeder MAX TPH Calibration Error

Gasious ?

PAH's
Run 2

Lehman - Roberts

09-03-91

12:45:53

Plant Status Report

* Rate Units Total Units *

* Production 356 Tons Per Hour 1644 Tons *

* Aggregate 285 Tons Per Hour 1269.9 Tons *

* Total A.C. 18.5 Tons Per Hour *

* Virgin A.C. 16.4 Tons Per Hour 74.37 Tons *

* R.A.P. A.C. 2.1 Tons Per Hour *

* R.A.P. 52 Tons Per Hour 300.0 Tons *

* Additive 0 Lbs Per Hour *

Agg. Composite Moisture 4.6 % *

* Mix Temperature 308 Deg. Sling. Position 42 % *

* A.C. Temperature 301 Deg. Burner Position 57 % *

Damper Position 66 % *

* Stack Temperature 261 Deg. *

B/H Pulse Time 20 Seconds *

* Instant Actual A.C. 5.19 % Negative Press 0.13 Inches *

* Average Actual A.C. 5.29 % B/H Diff. Press 4.2 Inches *

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec *

* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec *

* Feeder # 3 6.6 Mix % 15.7 Moist % *

* Feeder # 4 0.0 Mix % 13.7 Moist % *

* Feeder # 5 0.0 Mix % 2.7 Moist % *

* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg *

* Feeder # 7 28.4 Mix % 4.9 Moist % *

* R.A.P. 14.2 Mix % 6.2 Moist % 4.0 A.C. % *

* A.C. 5.3 Mix % *

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-03-91

12:46:18

Plant Status Report

	Rate	Units	Total	Units
Production	358	Tons Per Hour	1647	Tons
Aggregate	288	Tons Per Hour	1271.8	Tons
Total A.C.	18.7	Tons Per Hour		
Virgin A.C.	16.6	Tons Per Hour	74.48	Tons
R.A.P. A.C.	2.1	Tons Per Hour		
R.A.P.	51	Tons Per Hour	300.6	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix	Temperature	306 Deg.	Sling Position	42 %
A.C.	Temperature	301 Deg.	Burner Position	60 %
			Damper Position	66 %
Stack	Temperature	260 Deg.		
			B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.22 %		Negative Press	0.13 Inches
Average Actual A.C.	5.27 %		B/H Diff. Press	4.2 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	6.2 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			

Total 100.0 %

Additive 0.00 Mix %

09-03-91 13:14:00 Feeder MAX TPH Calibration Error

09-03-91 13:24:26 Feeder MAX TPH Calibration Error

09-03-91 13:35:29 Bin #5 High

09-03-91 13:43:00 Feeder MAX TPH Calibration Error

09-03-91 14:22:51 Bin #5 High

*
 * Lehman - Roberts *
 * 09-03-91 14:23:33 *
 * Plant Status Report *
 *

	Rate	Units	Total	Units
* Production	376	Tons Per Hour	2307	Tons
* Aggregate	305	Tons Per Hour	1779.0	Tons
* Total A.C.	19.6	Tons Per Hour		
* Virgin A.C.	17.5	Tons Per Hour	104.12	Tons
* R.A.P. A.C.	2.1	Tons Per Hour		
* R.A.P.	51	Tons Per Hour	422.9	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %

* H.C. Temperature 304 Deg. Burner Position 59 %
 * Damper Position 74 %
 * Stack Temperature 262 Deg.
 * B/H Pulse Time 10 Seconds
 * Instant Actual A.C. 5.38 % Negative Press 0.13 Inches
 * Average Actual A.C. 5.24 % B/H Diff. Press 3.6 Inches

* Running Mix # 51
 * Name : 411-E
 * Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Sec
1	9.5	3.4	A.C.	245	200	245
2	0.0	2.5	A.C.			200
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					

Total	100.0 %		Additive	0.00		Mix %

 * Lehman - Roberts
 * 09-03-91 14:32:55
 * Plant Status Report

	Rate	Units	Total	Units
Production	373	Tons Per Hour	2367	Tons
Aggregate	300	Tons Per Hour	1826.0	Tons
Total A.C.	19.8	Tons Per Hour		
Virgin A.C.	17.6	Tons Per Hour	106.86	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	53	Tons Per Hour	434.3	Tons
Additive	0	Lbs Per Hour		

Agg. Composite Moisture 4.6 %

* Mix Temperature 314 Deg. Sling. Position 26 %
 * A.C. Temperature 304 Deg. Burner Position 58 %
 * Damper Position 74 %
 * Stack Temperature 257 Deg.
 * B/H Pulse Time 10 Seconds
 * Instant Actual A.C. 5.30 % Negative Press 0.12 Inches
 * Average Actual A.C. 5.29 % B/H Diff. Press 2.7 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				
Total		100.0 %	Additive	0.00 Mix %	

Lehman - Roberts
 09-03-91 14:42:55
 Plant Status Report

	Rate	Units	Total	Units
Production	377	Tons Per Hour	2433	Tons
Aggregate	301	Tons Per Hour	1876.1	Tons
Total A.C.	20.1	Tons Per Hour		
Virgin A.C.	17.8	Tons Per Hour	109.80	Tons
R.A.P. A.C.	2.3	Tons Per Hour		
R.A.P.	56	Tons Per Hour	446.6	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix	Temperature	305 Deg.	Sling. Position	26 %
A.C.	Temperature	305 Deg.	Burner Position	60 %
			Damper Position	74 %
Stack	Temperature	257 Deg.		
			B/H Pulse Time	10 Seconds
Instant Actual A.C.	5.31 %		Negative Press	0.13 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	3.7 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

```

* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
* -----
* Total 100.0 % Additive 0.00 Mix %

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09-03-91 14:49:15 Bin #3 High

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*****
*
* Lehman - Roberts
* 09-03-91 14:52:56
* Plant Status Report
*

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*****
* Rate Units Total Units
* -----
* Production 381 Tons Per Hour 2498 Tons
* Aggregate 307 Tons Per Hour 1926.4 Tons
* Total A.C. 20.0 Tons Per Hour
* Virgin A.C. 17.8 Tons Per Hour 112.76 Tons
*
* R.A.P. A.C. 2.2 Tons Per Hour
*
* R.A.P. 54 Tons Per Hour 458.8 Tons
*
* Additive 0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 312 Deg. Sling. Position 26 %
* A.C. Temperature 305 Deg. Burner Position 55 %
* Damper Position 70 %
*
* Stack Temperature 257 Deg.
*
* B/H Pulse Time 10 Seconds
* Instant Actual A.C. 5.24 % Negative Press 0.10 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 3.4 Inches

```

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*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
* -----

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```

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 0.5 Moist % 0.0 Off Time 000 Sec

```


09-03-91

Lehman - Roberts

15:22:56

Plant Status Report

	Rate	Units	Total	Units
Production	372	Tons Per Hour	2694	Tons
Aggregate	298	Tons Per Hour	2077.1	Tons
Total A.C.	19.7	Tons Per Hour		
Virgin A.C.	17.5	Tons Per Hour	121.58	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	54	Tons Per Hour	495.1	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix	Temperature	313 Deg.	Sling. Position	26 %
A.C.	Temperature	305 Deg.	Burner Position	59 %
			Damper Position	72 %
Stack	Temperature	256 Deg.		
			B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.29 %		Negative Press	0.11 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	4.5 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Sec
1	9.5	3.4	A.C.	On Time	245	245 Sec
2	0.0	2.5	A.C.	Off Time	200	200 Sec
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total		100.0 %	Additive	0.00	Mix %	

* A.C. 5.3 Mix %

* Total 100.0 %

* Additive 0.00 Mix %

09-03-91 Lehman - Roberts 15:12:56
Plant Status Report

	Rate	Units	Total	Units
* Production	377	Tons Per Hour	2629	Tons
* Aggregate	305	Tons Per Hour	2027.1	Tons
* Total A.C.	20.0	Tons Per Hour		
* Virgin A.C.	17.9	Tons Per Hour	118.64	Tons
* R.A.P. A.C.	2.1	Tons Per Hour		
* R.A.P.	52	Tons Per Hour	482.8	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix Temperature	306	Deg.	Sling. Position	26 %
* A.C. Temperature	305	Deg.	Burner Position	59 %
			Damper Position	70 %
* Stack Temperature	254	Deg.		
			B/H Pulse Time	20 Seconds
* Instant Actual A.C.	5.30	%	Negative Press	0.10 Inches
* Average Actual A.C.	5.29	%	B/H Diff. Press	4.1 Inches

Running Mix # 51
Name : 411-E
Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
* Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
* Feeder # 3	6.6 Mix %	15.7 Moist %		
* Feeder # 4	0.0 Mix %	13.7 Moist %		
* Feeder # 5	0.0 Mix %	2.7 Moist %		
* Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
* Feeder # 7	28.4 Mix %	4.9 Moist %		
* R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. X	
* A.C.	5.3 Mix %			

* Total 100.0 %

* Additive 0.00 Mix %

Plant Status Report

	Rate	Units	Total	Units
Production	379	Tons Per Hour	2745	Tons
Aggregate	304	Tons Per Hour	2116.1	Tons
Total A.C.	20.1	Tons Per Hour		
Virgin A.C.	17.9	Tons Per Hour	123.84	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	55	Tons Per Hour	504.6	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix Temperature	294	Deg.	Sling. Position	31 %
A.C. Temperature	305	Deg.	Burner Position	62 %
			Damper Position	66 %
Stack Temperature	251	Deg.	B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.30	%	Negative Press	0.08 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	3.8 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C.	On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C.	Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %				
Feeder # 4	0.0	Mix %	13.7	Moist %				
Feeder # 5	0.0	Mix %	2.7	Moist %				
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set		320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %				
R.A.P.	14.2	Mix %	7.5	Moist %	4.0	A.C. %		
A.C.	5.3	Mix %						
Total		100.0 %	Additive		0.00	Mix %		

Running Mix # 3
Name : 307-AS
Description : 307-AS LIMESTONE

Feeder # 1	5.7 Mix %	3.4 Moist %	A.C.	On Time	210 Sec
Feeder # 2	29.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	0.0 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	62.0 Mix %	2.7 Moist %			
Feeder # 6	0.0 Mix %	2.6 Moist %	Mix Temp Set		250 Deg
Feeder # 7	0.0 Mix %	4.9 Moist %			

R.A.P.	0.0 Mix %	7.5 Moist %	4.0 A.C. %
A.C.	3.3 Mix %		

Total 100.0 % Additive 0.00 Mix %

09-03-91 15:32:17 Change Mix On

09-03-91 15:33:39 Bin #5 High

Gaseous & Part
 Run 3

 * Lehman - Roberts *
 * 09-03-91 16:39:58 *
 * Plant Status Report *
 * *****

	Rate	Units	Total	Units
Production	379	Tons Per Hour	3183	Tons
Aggregate	304	Tons Per Hour	2505.3	Tons
Total A.C.	19.8	Tons Per Hour		
Virgin A.C.	17.6	Tons Per Hour	140.53	Tons
R.A.P. A.C.	2.2	Tons Per Hour		
R.A.P.	55	Tons Per Hour	537.4	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix Temperature	308	Deg.	Sling. Position	24 %
A.C. Temperature	307	Deg.	Burner Position	77 %
			Damper Position	79 %
Stack Temperature	272	Deg.	B/H Pulse Time	10 Seconds
Instant Actual A.C.	5.21	%	Negative Press	0.28 Inches
Average Actual A.C.	5.30	%	B/H Diff. Press	3.8 Inches

 * Running Mix # 51 *
 * Name : 411-E *
 * Description : 411-E/W RAP AC IN RAP 3.5% *
 * *****

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			
Total 100.0 %		Additive 0.00 Mix %		

Lehman - Roberts

09-03-91

16:49:56

Plant Status Report

	Rate	Units	Total	Units
Production	364	Tons Per Hour	3248	Tons
Aggregate	296	Tons Per Hour	2555.3	Tons
Total A.C.	19.6	Tons Per Hour		
Virgin A.C.	17.7	Tons Per Hour	143.47	Tons
R.A.P. A.C.	1.9	Tons Per Hour		
R.A.P.	48	Tons Per Hour	549.5	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	324	Deg.	Sling Position	24 %
A.C. Temperature	307	Deg.	Burner Position	78 %
Stack Temperature	264	Deg.	Damper Position	73 %
			B/H Pulse Time	10 Seconds
Instant Actual A.C.	5.34	%	Negative Press	0.25 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	3.6 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C.	On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C.	Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %				
Feeder # 4	0.0	Mix %	13.7	Moist %				
Feeder # 5	0.0	Mix %	2.7	Moist %				
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set		320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %				
R.A.P.	14.2	Mix %	7.5	Moist %	4.0	A.C. %		
A.C.	5.3	Mix %						
Total	100.0	%			Additive	0.00	Mix %	

Lehman - Roberts

09-03-91

16:59:59

Plant Status Report

	Rate	Units	Total	Units
Production	369	Tons Per Hour	3315	Tons
Aggregate	298	Tons Per Hour	2605.5	Tons
Total A.C.	19.6	Tons Per Hour		
Virgin A.C.	17.5	Tons Per Hour	146.43	Tons
R.A.P. A.C.	2.0	Tons Per Hour		
R.A.P.	51	Tons Per Hour	561.9	Tons
Additive	0	Lbs Per Hour		
Agg. Composite Moisture				4.6 %
Mix Temperature	316	Deg.	Sling. Position	24 %
A.C. Temperature	307	Deg.	Burner Position	78 %
Stack Temperature	268	Deg.	Damper Position	79 %
Instant Actual A.C.	5.29	%	B/H Pulse Time	10 Seconds
Average Actual A.C.	5.29	%	Negative Press	0.28 Inches
			B/H Diff. Press	3.9 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C. On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C. Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %			
Feeder # 4	0.0	Mix %	13.7	Moist %			
Feeder # 5	0.0	Mix %	2.7	Moist %			
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set	320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %			
R.A.P.	14.2	Mix %	7.5	Moist %	4.0	A.C. %	
A.C.	5.3	Mix %					
Total		100.0 %	Additive		0.00	Mix %	

09-03-91

Lehman - Roberts

17:09:59

Plant Status Report

	Rate	Units	Total	Units
Production	383	Tons Per Hour	3380	Tons
Aggregate	310	Tons Per Hour	2656.0	Tons
Total A.C.	20.0	Tons Per Hour		

```

* R.A.P. A.C. 2.2 Tons Per Hour
* R.A.P. 53 Tons Per Hour 574.2 Tons
* Additive 0 Lbs Per Hour
* Agg. Composite Moisture 4.6 %
* Mix Temperature 325 Deg. Sling. Position 24 %
* A.C. Temperature 307 Deg. Burner Position 81 %
* Stack Temperature 270 Deg. Damper Position 75 %
* B/H Pulse Time 10 Seconds
* Instant Actual A.C. 5.22 % Negative Press 0.24 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 3.8 Inches

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*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Sec
1	9.5	3.4	A.C.	245		245
2	0.0	2.5	A.C.		200	200
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total		100.0 %	Additive	0.00		Mix %

09-03-91 17:16:14 Bin #5 High

```

*****
* Lehman - Roberts
* 09-03-91 17:19:57
* Plant Status Report

```

	Rate	Units	Total	Units
Production	373	Tons Per Hour	3445	Tons
Aggregate	301	Tons Per Hour	2706.2	Tons
Total A.C.	19.7	Tons Per Hour		
Virgin A.C.	17.6	Tons Per Hour	152.30	Tons

* R.A.P. 52 Tons Per Hour 586.2 Tons

* Additive 0 Lbs Per Hour

* Agg. Composite Moisture 4.6 %

* Mix Temperature 321 Deg. Sling. Position 24 %

* A.C. Temperature 307 Deg. Burner Position 76 %

* Stack Temperature 272 Deg. Damper Position 84 %

* B/H Pulse Time 10 Seconds

* Instant Actual A.C. 5.28 % Negative Press 0.20 Inches

* Average Actual A.C. 5.29 % B/H Diff. Press 4.1 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			

Total	100.0 %		Additive	0.00 Mix %

09-03-91 17:28:39 Bin #4 High

Lehman - Roberts

09-03-91 17:29:59

Plant Status Report

	Rate	Units	Total	Units
Production	370	Tons Per Hour	3511	Tons
Aggregate	298	Tons Per Hour	2756.2	Tons
Total A.C.	19.7	Tons Per Hour		
Virgin A.C.	17.6	Tons Per Hour	155.26	Tons

```

* R.A.P.      52   Tons Per Hour      598.2   Tons
*
* Additive    0   Lbs Per Hour
*
* Agg. Composite Moisture  4.6 %
*
* Mix Temperature  308 Deg.   Sling. Position  24 %
* A.C. Temperature  308 Deg.   Burner Position  73 %
*                               Damper Position  78 %
*
* Stack Temperature  257 Deg.
*                               B/H Pulse Time  15   Seconds
*
* Instant Actual A.C.  5.33 %   Negative Press  0.19 Inches
* Average Actual A.C.  5.29 %   B/H Diff. Press  4.3   Inches

```

```

*
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

```

* Feeder # 1   9.5 Mix %   3.4 Moist %   A.C. On Time  245 Sec
* Feeder # 2   0.0 Mix %   2.5 Moist %   A.C. Off Time 200 Sec
* Feeder # 3   6.6 Mix %   15.7 Moist %
* Feeder # 4   0.0 Mix %   13.7 Moist %
* Feeder # 5   0.0 Mix %   2.7 Moist %
* Feeder # 6  36.0 Mix %   2.6 Moist %   Mix Temp Set  320 Deg
* Feeder # 7  28.4 Mix %   4.9 Moist %

```

```

* R.A.P.      14.2 Mix %   7.5 Moist %   4.0 A.C. %
*
* A.C.        5.3 Mix %

```

```

* -----
* Total      100.0 %
*
* Additive   0.00 Mix %

```

09-03-91 17:31:00 Rotary Batcher Not Located

09-03-91 17:31:17 Rotary Batcher Not Located

09-03-91 17:31:34 Bin Top Conveyor Right Overtravel

	Rate	Units	Total	Units
* Production	400	Tons Per Hour	3576	Tons
* Aggregate	328	Tons Per Hour	2807.2	Tons
* Total A.C.	20.0	Tons Per Hour		
* Virgin A.C.	17.9	Tons Per Hour	158.20	Tons
* R.A.P. A.C.	2.1	Tons Per Hour		
* R.A.P.	52	Tons Per Hour	610.6	Tons
* Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
* Mix	Temperature	301 Deg.	Sling. Position	24 %
* A.C.	Temperature	309 Deg.	Burner Position	76 %
				Damper Position 75 %
* Stack	Temperature	255 Deg.	B/H Pulse Time	15 Seconds
* Instant Actual A.C.	5.00 %		Negative Press	0.21 Inches
* Average Actual A.C.	5.29 %		B/H Diff. Press	4.3 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
* Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
* Feeder # 3	6.6 Mix %	15.7 Moist %		
* Feeder # 4	0.0 Mix %	13.7 Moist %		
* Feeder # 5	0.0 Mix %	2.7 Moist %		
* Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
* Feeder # 7	28.4 Mix %	4.9 Moist %		
* R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
* A.C.	5.3 Mix %			

* Total	100.0 %		Additive	0.00 Mix %

09-03-91 17:43:40 Bin #2 Low

	Rate	Units	Total	Units
* Production	371	Tons Per Hour	3606	Tons
* Aggregate	300	Tons Per Hour	2830.1	Tons
* Total A.C.	19.6	Tons Per Hour		
* Virgin A.C.	17.7	Tons Per Hour	159.55	Tons
* R.A.P. A.C.	2.1	Tons Per Hour		
* R.A.P.	51	Tons Per Hour	616.2	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix Temperature	314	Deg.	Sling. Position	24 %
* A.C. Temperature	309	Deg.	Burner Position	72 %
			Damper Position	79 %
* Stack Temperature	264	Deg.		
			B/H Pulse Time	15 Seconds
* Instant Actual A.C.	5.33	%	Negative Press	0.21 Inches
* Average Actual A.C.	5.29	%	B/H Diff. Press	4.5 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
* Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
* Feeder # 3	6.6 Mix %	15.7 Moist %		
* Feeder # 4	0.0 Mix %	13.7 Moist %		
* Feeder # 5	0.0 Mix %	2.7 Moist %		
* Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
* Feeder # 7	28.4 Mix %	4.9 Moist %		
* R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
* A.C.	5.3 Mix %			

* Total	100.0 %		Additive	0.00 Mix %

Run 1

Formaldehyde

09-30-91 09:56:25 Bin #5 High

09-30-91 10:29:40 Bin #5 Low

09-30-91 10:36:22 Feeder MAX TPH Calibration Error

09-30-91 10:37:18 Bin #4 High

Lehman - Roberts

09-30-91

10:50:51

Plant Status Report

	Rate	Units	Total	Units
* Production	299	Tons Per Hour	682	Tons
* Aggregate	242	Tons Per Hour	527.2	Tons
* Total A.C.	15.8	Tons Per Hour		
* Virgin A.C.	14.2	Tons Per Hour	30.78	Tons
* R.A.P. A.C.	1.6	Tons Per Hour		
* R.A.P.	40	Tons Per Hour	125.4	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix Temperature	314	Deg.	Sling. Position	70 %
* A.C. Temperature	297	Deg.	Burner Position	35 %
			Damper Position	55 %
* Stack Temperature	248	Deg.		
* Instant Actual A.C.	5.28	%	B/H Pulse Time	35 Seconds
* Average Actual A.C.	5.28	%	Negative Press	0.18 Inches
			B/H Diff. Press	3.5 Inches

Running Mix # 51

```

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
*
*
* Total 100.0 % Additive 0.00 Mix %

```

```

*****
*
* Lehman - Roberts
* 09-30-91 11:00:17
* Plant Status Report
*
*****

```

```

*****
* Rate Units Total Units
*-----
* Production 304 Tons Per Hour 731 Tons
* Aggregate 244 Tons Per Hour 565.1 Tons
* Total A.C. 16.1 Tons Per Hour
* Virgin A.C. 14.3 Tons Per Hour 33.02 Tons
*
* R.A.P. A.C. 1.8 Tons Per Hour
*
* R.A.P. 44 Tons Per Hour 134.2 Tons
*
* Additive 0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 320 Deg. Sling. Position 70 %
* A.C. Temperature 301 Deg. Burner Position 33 %
* Damper Position 55 %
*
* Stack Temperature 245 Deg.
*
* B/H Pulse Time 35 Seconds
* Instant Actual A.C. 5.29 % Negative Press 0.18 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 3.6 Inches
*
*****

```

```

* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*
*****

```

```

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %

```

```

* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
* A.C. 5.3 Mix %
*
* -----
* Total 100.0 % Additive 0.00 Mix %

```

09-30-91 11:01:58 Feeder MAX TPH Calibration Error

09-30-91 11:06:31 Bin #4 Low

```

*****
*                               Lehman - Roberts                               *
* 09-30-91                               11:10:17                               *
*                               Plant Status Report                               *
*****

```

	Rate	Units	Total	Units
* Production	295	Tons Per Hour	785	Tons
* Aggregate	237	Tons Per Hour	605.6	Tons
* Total A.C.	15.7	Tons Per Hour		
* Virgin A.C.	14.0	Tons Per Hour	35.37	Tons
* R.A.P. A.C.	1.6	Tons Per Hour		
* R.A.P.	42	Tons Per Hour	143.8	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix	Temperature	331 Deg.	Sling. Position	70 %
* A.C.	Temperature	303 Deg.	Burner Position	30 %
			Damper Position	55 %
* Stack	Temperature	254 Deg.	B/H Pulse Time	35 Seconds
* Instant Actual A.C.	5.30 %		Negative Press	0.18 Inches
* Average Actual A.C.	5.29 %		B/H Diff. Press	3.6 Inches

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*****

```

```

* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec *
* Feeder # 3 6.6 Mix % 15.7 Moist % *
* Feeder # 4 0.0 Mix % 13.7 Moist % *
* Feeder # 5 0.0 Mix % 2.7 Moist % *
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg *
* Feeder # 7 29.4 Mix % 4.9 Moist % *
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. % *
*
* A.C. 5.3 Mix % *
*
* ----- *
* Total 100.0 % Additive 0.00 Mix % *
*
* *****

```

09-30-91 11:11:45 Bin #5 High

09-30-91 11:17:43 Feeder MAX TPH Calibration Error

```

*****
*
* Lehman - Roberts
* 09-30-91 11:20:17
* Plant Status Report-
*
*****

```

```

* Rate Units Total Units
* -----
* Production 296 Tons Per Hour 835 Tons
* Aggregate 240 Tons Per Hour 645.3 Tons
* Total A.C. 15.5 Tons Per Hour
* Virgin A.C. 13.9 Tons Per Hour 37.71 Tons
*
* R.A.P. A.C. 1.6 Tons Per Hour
*
* R.A.P. 40 Tons Per Hour 153.2 Tons
*
* Additive 0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 322 Deg. Sling. Position 70 %
* A.C. Temperature 304 Deg. Burner Position 33 %
* Damper Position 55 %
*
* Stack Temperature 249 Deg.
*
* B/H Pulse Time 35 Seconds
* Instant Actual A.C. 5.23 % Negative Press 0.19 Inches
* Average Actual A.C. 5.29 % B/H Diff. Press 3.4 Inches
*
*****

```


Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				
Total		100.0 %	Additive	0.00 Mix %	

Lehman - Roberts
 09-30-91 11:30:18
 Plant Status Report

	Rate	Units	Total	Units
Production	298	Tons Per Hour	888	Tons
Aggregate	241	Tons Per Hour	686.2	Tons
Total A.C.	15.6	Tons Per Hour		
Virgin A.C.	14.0	Tons Per Hour	40.10	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	41	Tons Per Hour	162.7	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	323	Deg.	Sling. Position	70 %
A.C. Temperature	304	Deg.	Burner Position	33 %
			Damper Position	55 %
Stack Temperature	254	Deg.	B/H Pulse Time	35 Seconds
Instant Actual A.C.	5.25	%	Negative Press	0.17 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	3.6 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec

```

* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
* -----
* Total 100.0 % Additive 0.00 Mix %
*
*****

```

```

*****
*
* Lehman - Roberts
* 09-30-91 11:40:18
* Plant Status Report
*
*****

```

	Rate	Units	Total	Units
Production	297	Tons Per Hour	941	Tons
Aggregate	239	Tons Per Hour	725.8	Tons
Total A.C.	13.8	Tons Per Hour		
Virgin A.C.	14.1	Tons Per Hour	42.45	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	42	Tons Per Hour	172.1	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	328	Deg.	Sling. Position	70 %
A.C. Temperature	304	Deg.	Burner Position	34 %
			Damper Position	55 %
Stack Temperature	259	Deg.	B/H Pulse Time	35 Seconds
Instant Actual A.C.	5.31	%	Negative Press	0.18 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	3.6 Inches

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%
*

```

```

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %

```

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-30-91

11:50:19

Plant Status Report

	Rate	Units	Total	Units
Production	292	Tons Per Hour	992	Tons
Aggregate	237	Tons Per Hour	766.4	Tons
Total A.C.	15.8	Tons Per Hour		
Virgin A.C.	14.2	Tons Per Hour	44.82	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	39	Tons Per Hour	181.6	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix	Temperature	317 Deg.	Sling. Position	70 %
A.C.	Temperature	304 Deg.	Burner Position	34 %
			Damper Position	55 %
Stack	Temperature	257 Deg.	B/H Pulse Time	35 Seconds
Instant Actual A.C.	5.39 %		Negative Press	0.18 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	3.6 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			

Total 100.0 %

Additive 0.00 Mix %

09-30-91

Lehman - Roberts

12:00:18

Plant Status Report

	Rate	Units	Total	Units
Production	296	Tons Per Hour	1043	Tons
Aggregate	238	Tons Per Hour	806.2	Tons
Total A.C.	15.7	Tons Per Hour		
Virgin A.C.	14.0	Tons Per Hour	47.16	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	42	Tons Per Hour	190.9	Tons
Additive	0	Lbs Per Hour		
Agg. Composite Moisture				4.6 %
Mix Temperature	323	Deg.	Sling Position	70 %
A.C. Temperature	305	Deg.	Burner Position	31 %
Stack Temperature	250	Deg.	Damper Position	55 %
Instant Actual A.C.	5.30	%	B/H Pulse Time	35 Seconds
Average Actual A.C.	5.29	%	Negative Press	0.21 Inches
			B/H Diff. Press	3.7 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Temp
1	9.5	3.4	A.C.	245	245	320 Deg
2	0.0	2.5	A.C.	200	200	
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total		100.0 %	Additive	0.00	Mix %	

09-30-91 12:05:43 Main Flame Failure

09-30-91 12:05:45 Asphalt Valve Recirculate

09-30-91 12:05:47 System Stop

09-30-91 12:11:14 System Start

09-30-91 12:11:16 Preheat Starting

09-30-91 12:14:46 Feeder MAX TPH Calibration Error

09-30-91 12:16:22 Asphalt Deviation

09-30-91 12:17:09 Asphalt Deviation

*
* Lehman - Roberts *
* 09-30-91 12:22:05 *
* Plant Status Report *
*

	Rate	Units	Total	Units
* Production	290	Tons Per Hour	1124	Tons
* Aggregate	235	Tons Per Hour	868.1	Tons

* R.A.P. A.C. 1.6 Tons Per Hour *
 * R.A.P. 40 Tons Per Hour 205.6 Tons *
 * Additive 0 Lbs Per Hour *
 * Agg. Composite Moisture 4.6 % *
 * Mix Temperature 321 Deg. Sling. Position 70 % *
 * A.C. Temperature 304 Deg. Burner Position 30 % *
 * Damper Position 55 % *
 * Stack Temperature 261 Deg. *
 * B/H Pulse Time 35 Seconds *
 * Instant Actual A.C. 5.31 % Negative Press 0.20 Inches *
 * Average Actual A.C. 34.04 % B/H Diff. Press 3.7 Inches *

* Running Mix # 51 *
 * Name : 411-E *
 * Description : 411-E/W RAP AC IN RAP 3.5% *

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Temp
1	9.5	3.4		245		
2	0.0	2.5		200		
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6				320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total 100.0 %		Additive 0.00 Mix %				

 * Lehman - Roberts *
 * 09-30-91 12:32:06 *
 * Plant Status Report *

	Rate	Units	Total	Units
Production	300	Tons Per Hour	1175	Tons
Aggregate	243	Tons Per Hour	908.6	Tons
Total A.C.	15.8	Tons Per Hour		
Virgin A.C.	14.3	Tons Per Hour	53.21	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	41	Tons Per Hour	214.7	Tons

Agg. Composite Moisture 4.6 %

Mix Temperature 326 Deg. Sling. Position 70 %
A.C. Temperature 305 Deg. Burner Position 34 %
Damper Position 55 %

Stack Temperature 249 Deg. B/H Pulse Time 35 Seconds
Instant Actual A.C. 5.30 % Negative Press 0.18 Inches
Average Actual A.C. 5.29 % B/H Diff. Press 3.6 Inches

Running Mix # 51
Name : 411-E
Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			

Total 100.0 % Additive 0.00 Mix %

Lehman - Roberts

09-30-91

12:32:24

Plant Status Report

	Rate	Units	Total	Units
Production	298	Tons Per Hour	1177	Tons
Aggregate	241	Tons Per Hour	909.7	Tons
Total A.C.	15.7	Tons Per Hour		
Virgin A.C.	14.1	Tons Per Hour	53.28	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	41	Tons Per Hour	215.0	Tons
Additive	0	Lbs Per Hour		

Agg. Composite Moisture 4.6 %

Mix Temperature 326 Deg. Sling. Position 70 %
A.C. Temperature 305 Deg. Burner Position 34 %
Damper Position 55 %

* Instant Actual A.C. 5.28 % Negative Press 0.17 Inches *
 * Average Actual A.C. 5.35 % B/H Diff. Press 3.5 Inches *

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				

Total 100.0 % Additive 0.00 Mix %

RUN 2

Formaldehyde

09-30-91

Lehman - Roberts

13:30:37

Plant Status Report

	Rate	Units	Total	Units
Production	307	Tons Per Hour	1481	Tons
Aggregate	248	Tons Per Hour	1139.1	Tons
Total A.C.	16.1	Tons Per Hour		
Virgin A.C.	14.4	Tons Per Hour	66.51	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	43	Tons Per Hour	275.5	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix	Temperature	319 Deg.	Sling. Position	70 %
A.C.	Temperature	314 Deg.	Burner Position	37 %
			Damper Position	59 %
Stack	Temperature	270 Deg.		
			B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.24 %		Negative Press	0.25 Inches
Average Actual A.C.	5.30 %		B/H Diff. Press	3.4 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				
Total 100.0 %		Additive 0.00 Mix %			

Lehman - Roberts

09-30-91

13:40:06

Plant Status Report

	Rate	Units	Total	Units
Production	300	Tons Per Hour	1530	Tons
Aggregate	241	Tons Per Hour	1176.8	Tons
Total A.C.	15.9	Tons Per Hour		
Virgin A.C.	14.2	Tons Per Hour	68.76	Tons
R.A.P. A.C.	1.8	Tons Per Hour		
R.A.P.	43	Tons Per Hour	284.7	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix Temperature		318 Deg.	Sling. Position	70 %
A.C. Temperature		314 Deg.	Burner Position	34 %
			Damper Position	57 %
Stack Temperature		266 Deg.		
			B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.31 %		Negative Press	0.22 Inches
Average Actual A.C.	5.29 %		B/H Diff. Press	3.3 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	/ 320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			
Total 100.0 %		Additive 0.00 Mix %		

09-30-91

Lehman - Roberts
Plant Status Report

13:50:05

	Rate	Units	Total	Units
Production	299	Tons Per Hour	1582	Tons
Aggregate	243	Tons Per Hour	1217.4	Tons
Total A.C.	15.8	Tons Per Hour		
Virgin A.C.	14.2	Tons Per Hour	71.12	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	40	Tons Per Hour	294.3	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix Temperature	330	Deg.	Sling. Position	70 %
A.C. Temperature	315	Deg.	Burner Position	33 %
			Damper Position	57 %
Stack Temperature	259	Deg.	B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.28	%	Negative Press	0.22 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	3.1 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			
Total 100.0 %		Additive 0.00 Mix %		

09-30-91

Lehman - Roberts
Plant Status Report

14:00:06

```

* Production      302 Tons Per Hour      1634 Tons
* Aggregate      245 Tons Per Hour      1257.2 Tons
* Total A.C.     15.6 Tons Per Hour
* Virgin A.C.    14.0 Tons Per Hour      73.48 Tons
*
* R.A.P. A.C.    1.6 Tons Per Hour
*
* R.A.P.         41 Tons Per Hour      303.8 Tons
*
* Additive       0 Lbs Per Hour
*
* Agg. Composite Moisture 4.6 %
*
* Mix Temperature 329 Deg.      Sling. Position 70 %
* A.C. Temperature 314 Deg.      Burner Position 37 %
*
* Stack Temperature 270 Deg.      Damper Position 57 %
*
* Instant Actual A.C. 5.16 %      B/H Pulse Time 20 Seconds
* Average Actual A.C. 5.28 %      Negative Press 0.20 Inches
* B/H Diff. Press 3.1 Inches

```

```

*****
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

```

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec
* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec
* Feeder # 3 6.6 Mix % 15.7 Moist %
* Feeder # 4 0.0 Mix % 13.7 Moist %
* Feeder # 5 0.0 Mix % 2.7 Moist %
* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg
* Feeder # 7 28.4 Mix % 4.9 Moist %
*
* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
*
* A.C. 5.3 Mix %
*
* Total 100.0 % Additive 0.00 Mix %

```

```

09-30-91 14:07:02 Bin #5 High

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```

*****
* Lehman - Roberts
* 09-30-91 14:10:06
* Plant Status Report

```

```

* Production      294   Tons Per Hour      1686   Tons
* Aggregate      236   Tons Per Hour      1297.7 Tons
* Total A.C.     15.8 Tons Per Hour
* Virgin A.C.    14.1 Tons Per Hour      75.84 Tons
*
* R.A.P. A.C.    1.7 Tons Per Hour
*
* R.A.P.         42   Tons Per Hour      313.3 Tons
*
* Additive       0    Lbs Per Hour
*
*                               Agg. Composite Moisture  4.6 %
*
* Mix Temperature 338 Deg.   Sling. Position  70 %
* A.C. Temperature 315 Deg.   Burner Position  31 %
*                               Damper Position  57 %
*
* Stack Temperature 254 Deg.
*                               B/H Pulse Time    20   Seconds
* Instant Actual A.C. 5.37 %   Negative Press   0.21 Inches
* Average Actual A.C. 5.29 %   B/H Diff. Press  3.2  Inches

```

```

* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

```

* Feeder # 1  9.5 Mix %   3.4 Moist %   A.C.   On Time 245 Sec
* Feeder # 2  0.0 Mix %   2.5 Moist %   A.C.   Off Time 200 Sec
* Feeder # 3  6.6 Mix %   15.7 Moist %
* Feeder # 4  0.0 Mix %   13.7 Moist %
* Feeder # 5  0.0 Mix %   2.7 Moist %
* Feeder # 6  36.0 Mix %  2.6 Moist %   Mix Temp Set  320 Deg
* Feeder # 7  28.4 Mix %  4.9 Moist %
*
* R.A.P.      14.2 Mix %   7.5 Moist %   4.0 A.C. %
*
* A.C.        5.3 Mix %

```

```

* -----
* Total 100.0 %           Additive 0.00 Mix %

```

```

*
* Lehman - Roberts
* 09-30-91 14:20:06
* Plant Status Report

```

```

*
* Rate Units Total Units
*-----
* Production 325 Tons Per Hour 1738 Tons
* Aggregate  249 Tons Per Hour 1337.8 Tons
* Total A.C.  16.0 Tons Per Hour
* Virgin A.C. 14.4 Tons Per Hour  78.20 Tons

```

```

* R.A.P.          40   Tons Per Hour          322.5   Tons
*
* Additive        0    Lbs Per Hour
*
* Agg. Composite Moisture  4.6 %
*
* Mix Temperature  306 Deg.   Sling. Position  70 %
* A.C. Temperature  317 Deg.   Burner Position  46 %
*                               Damper Position  57 %
*
* Stack Temperature  252 Deg.
*                               B/H Pulse Time   20   Seconds
*
* Instant Actual A.C.  5.24 %   Negative Press   0.17 Inches
* Average Actual A.C.  5.29 %   B/H Diff. Press  3.0   Inches

```

```

*****
*
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

```

* Feeder # 1    9.5 Mix %    3.4 Moist %    A.C.    On Time  245 Sec
* Feeder # 2    0.0 Mix %    2.5 Moist %    A.C.    Off Time  200 Sec
* Feeder # 3    6.6 Mix %    15.7 Moist %
* Feeder # 4    0.0 Mix %    13.7 Moist %
* Feeder # 5    0.0 Mix %    2.7 Moist %
* Feeder # 6    36.0 Mix %    2.6 Moist %    Mix Temp Set  320 Deg
* Feeder # 7    28.4 Mix %    4.9 Moist %
*
* R.A.P.       14.2 Mix %    7.5 Moist %    4.0 A.C. %
*
* A.C.         5.3 Mix %
*
* -----
* Total       100.0 %
* Additive    0.00 Mix %

```

```

*****
*
* Lehman - Roberts
* 09-30-91          14:30:06
* Plant Status Report

```

```

*****
*
* Rate Units          Total Units
* -----
* Production  298   Tons Per Hour    1790   Tons
* Aggregate   241   Tons Per Hour    1378.0 Tons
* Total A.C.  15.6 Tons Per Hour
* Virgin A.C. 14.0 Tons Per Hour    80.57 Tons
*
* R.A.P. A.C.   1.6 Tons Per Hour
*
* R.A.P.       41   Tons Per Hour    331.9 Tons
*
* Additive    0    Lbs Per Hour
*
* Agg. Composite Moisture  4.6 %

```

* A.C. Temperature 318 Deg. Burner Position 35 %
 * Damper Position 57 %
 * Stack Temperature 251 Deg.
 * B/H Pulse Time 20 Seconds
 * Instant Actual A.C. 5.23 % Negative Press 0.16 Inches
 * Average Actual A.C. 5.29 % B/H Diff. Press 3.0 Inches

 * Running Mix # 51
 * Name : 411-E
 * Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		

* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %
 * A.C. 5.3 Mix %

 * Total 100.0 % Additive 0.00 Mix %

09-30-91 14:39:22 Bin #4 High

 * Lehman - Roberts
 * 09-30-91 14:40:07
 * Plant Status Report

	Rate	Units	Total	Units
Production	300	Tons Per Hour	1842	Tons
Aggregate	243	Tons Per Hour	1418.4	Tons
Total A.C.	15.6	Tons Per Hour		
Virgin A.C.	14.0	Tons Per Hour	82.95	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	41	Tons Per Hour	341.3	Tons
Additive	0	Lbs Per Hour		

Agg. Composite Moisture 4.6 %

Stack Temperature 263 Deg. Damper Position 57 %
 B/H Pulse Time 20 Seconds
 Instant Actual A.C. 5.21 % Negative Press 0.20 Inches
 Average Actual A.C. 5.29 % B/H Diff. Press 3.3 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Temp
1	9.5	3.4	A.C.	245	245	
2	0.0	2.5	A.C.	200	200	
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					

Total 100.0 % Additive 0.00 Mix %

Lehman - Roberts
 09-30-91 14:50:06
 Plant Status Report

	Rate	Units	Total	Units
Production	298	Tons Per Hour	1893	Tons
Aggregate	241	Tons Per Hour	1458.4	Tons
Total A.C.	15.7	Tons Per Hour		
Virgin A.C.	14.1	Tons Per Hour	85.30	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	41	Tons Per Hour	350.7	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %

Mix Temperature 330 Deg. Sling. Position 70 %
 A.C. Temperature 320 Deg. Burner Position 34 %
 Damper Position 57 %
 Stack Temperature 259 Deg. B/H Pulse Time 20 Seconds
 Instant Actual A.C. 5.26 % Negative Press 0.23 Inches
 Average Actual A.C. 5.29 % B/H Diff. Press 3.2 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				

Total	100.0 %	Additive	0.00 Mix %		

09-30-91 14:53:47 Feeder MAX TPH Calibration Error

Lehman - Roberts

09-30-91

14:59:28

Plant Status Report

	Rate	Units	Total	Units
Production	297	Tons Per Hour	1942	Tons
Aggregate	238	Tons Per Hour	1496.3	Tons
Total A.C.	16.1	Tons Per Hour		
Virgin A.C.	14.3	Tons Per Hour	87.53	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	43	Tons Per Hour	359.7	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix Temperature	329	Deg.	Sling Position	70 %
A.C. Temperature	320	Deg.	Burner Position	35 %
			Damper Position	57 %
Stack Temperature	265	Deg.	B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.38	%	Negative Press	0.22 Inches
Average Actual A.C.	5.28	%	B/H Diff. Press	3.2 Inches

Name : 411-E
Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
* Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
* Feeder # 3	6.6 Mix %	15.7 Moist %			
* Feeder # 4	0.0 Mix %	13.7 Moist %			
* Feeder # 5	0.0 Mix %	2.7 Moist %			
* Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
* Feeder # 7	28.4 Mix %	4.9 Moist %			
* R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
* A.C.	5.3 Mix %				

Total 100.0 % Additive 0.00 Mix %

Formaldehyde

RUN 3

09-30-91

Lehman - Roberts

16:04:58

Plant Status Report

	Rate	Units	Total	Units
Production	299	Tons Per Hour	2016	Tons
Aggregate	243	Tons Per Hour	1553.8	Tons
Total A.C.	15.8	Tons Per Hour		
Virgin A.C.	14.3	Tons Per Hour	90.90	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	40	Tons Per Hour	371.2	Tons
Additive	0	Lbs Per Hour		
				Agg. Composite Moisture 4.6 %
Mix	Temperature	320 Deg.	Sling. Position	70 %
A.C.	Temperature	321 Deg.	Burner Position	44 %
			Damper Position	55 %
Stack	Temperature	251 Deg.		
			B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.33 %		Negative Press	0.16 Inches
Average Actual A.C.	5.32 %		B/H Diff. Press	2.8 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C.	On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C.	Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %			
Feeder # 4	0.0 Mix %	13.7 Moist %			
Feeder # 5	0.0 Mix %	2.7 Moist %			
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set		320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %			
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %		
A.C.	5.3 Mix %				

Total 100.0 % Additive 0.00 Mix %

Lehman - Roberts

09-30-91

16:14:06

Plant Status Report

Rate	Units	Total	Units
Production	305 Tons Per Hour	2063	Tons
Aggregate	250 Tons Per Hour	1590.6	Tons
Total A.C.	16.0 Tons Per Hour		
Virgin A.C.	14.4 Tons Per Hour	93.06	Tons
R.A.P. A.C.	1.6 Tons Per Hour		
R.A.P.	39 Tons Per Hour	379.5	Tons
Additive	0 Lbs Per Hour		
			Agg. Composite Moisture 4.6 %
Mix Temperature	324 Deg.	Sling. Position	70 %
A.C. Temperature	321 Deg.	Burner Position	37 %
Stack Temperature	248 Deg.	Damper Position	55 %
		B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.22 %	Negative Press	0.18 Inches
Average Actual A.C.	5.30 %	B/H Diff. Press	2.8 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			
Total 100.0 %		Additive 0.00 Mix %		

Lehman - Roberts

09-30-91

16:24:05

Plant Status Report

	Rate	Units	Total	Units
Production	290	Tons Per Hour	2115	Tons
Aggregate	234	Tons Per Hour	1631.2	Tons
Total A.C.	15.4	Tons Per Hour		
Virgin A.C.	13.8	Tons Per Hour	95.44	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	41	Tons Per Hour	388.7	Tons
Additive	0	Lbs Per Hour		
Agg. Composite Moisture				4.6 %
Mix Temperature	331	Deg.	Sling Position	70 %
A.C. Temperature	321	Deg.	Burner Position	35 %
			Damper Position	55 %
Stack Temperature	258	Deg.	B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.31	%	Negative Press	0.19 Inches
Average Actual A.C.	5.30	%	B/H Diff. Press	2.9 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5 Mix %	3.4 Moist %	A.C. On Time	245 Sec
Feeder # 2	0.0 Mix %	2.5 Moist %	A.C. Off Time	200 Sec
Feeder # 3	6.6 Mix %	15.7 Moist %		
Feeder # 4	0.0 Mix %	13.7 Moist %		
Feeder # 5	0.0 Mix %	2.7 Moist %		
Feeder # 6	36.0 Mix %	2.6 Moist %	Mix Temp Set	320 Deg
Feeder # 7	28.4 Mix %	4.9 Moist %		
R.A.P.	14.2 Mix %	7.5 Moist %	4.0 A.C. %	
A.C.	5.3 Mix %			

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-30-91

15:34:07

Plant Status Report

* Rate Units Total Units *

* Production 285 Tons Per Hour 2167 Tons *

* Aggregate 228 Tons Per Hour 1671.4 Tons *

* Total A.C. 15.5 Tons Per Hour *

* Virgin A.C. 13.9 Tons Per Hour 97.81 Tons *

* R.A.P. A.C. 1.6 Tons Per Hour *

* R.A.P. 41 Tons Per Hour 398.2 Tons *

* Additive 0 Lbs Per Hour *

Agg. Composite Moisture 4.6 % *

* Mix Temperature 337 Deg. Sling. Position 70 % *

* A.C. Temperature 321 Deg. Burner Position 33 % *

Damper Position 55 % *

* Stack Temperature 262 Deg. *

B/H Pulse Time 20 Seconds *

* Instant Actual A.C. 5.45 % Negative Press 0.21 Inches *

* Average Actual A.C. 5.29 % B/H Diff. Press 3.0 Inches *

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

* Feeder # 1 9.5 Mix % 3.4 Moist % A.C. On Time 245 Sec *

* Feeder # 2 0.0 Mix % 2.5 Moist % A.C. Off Time 200 Sec *

* Feeder # 3 6.6 Mix % 15.7 Moist % *

* Feeder # 4 0.0 Mix % 13.7 Moist % *

* Feeder # 5 0.0 Mix % 2.7 Moist % *

* Feeder # 6 36.0 Mix % 2.6 Moist % Mix Temp Set 320 Deg *

* Feeder # 7 28.4 Mix % 4.9 Moist % *

* R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. % *

* A.C. 5.3 Mix % *

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-30-91

16:44:06

Plant Status Report

	Rate	Units	Total	Units
Production	295	Tons Per Hour	2220	Tons
Aggregate	237	Tons Per Hour	1712.2	Tons
Total A.C.	15.9	Tons Per Hour		
Virgin A.C.	14.2	Tons Per Hour	100.19	Tons
R.A.P. A.C.	1.7	Tons Per Hour		
R.A.P.	42	Tons Per Hour	407.6	Tons
Additive	0	Lbs Per Hour		
Agg. Composite Moisture				4.6 %
Mix Temperature	329	Deg.	Sling Position	70 %
A.C. Temperature	321	Deg.	Burner Position	35 %
			Damper Position	55 %
Stack Temperature	260	Deg.	B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.38	%	Negative Press	2.17 Inches
Average Actual A.C.	5.29	%	B/H Diff. Press	3.0 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder # 1	9.5	Mix %	3.4	Moist %	A.C. On Time	245	Sec
Feeder # 2	0.0	Mix %	2.5	Moist %	A.C. Off Time	200	Sec
Feeder # 3	6.6	Mix %	15.7	Moist %			
Feeder # 4	0.0	Mix %	13.7	Moist %			
Feeder # 5	0.0	Mix %	2.7	Moist %			
Feeder # 6	36.0	Mix %	2.6	Moist %	Mix Temp Set	320	Deg
Feeder # 7	28.4	Mix %	4.9	Moist %			

R.A.P. 14.2 Mix % 7.5 Moist % 4.0 A.C. %

A.C. 5.3 Mix %

Total 100.0 %

Additive 0.00 Mix %

Lehman - Roberts

09-30-91

16:54:06

Plant Status Report

	Rate	Units	Total	Units
Production	295	Tons Per Hour	2271	Tons
Aggregate	238	Tons Per Hour	1752.1	Tons
Total A.C.	15.7	Tons Per Hour		
Virgin A.C.	14.1	Tons Per Hour	102.55	Tons
R.A.P. A.C.	1.6	Tons Per Hour		
R.A.P.	41	Tons Per Hour	416.9	Tons
Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
Mix	Temperature	323 Deg.	Sling. Position	70 %
A.C.	Temperature	321 Deg.	Burner Position	39 %
			Damper Position	55 %
Stack	Temperature	247 Deg.	B/H Pulse Time	20 Seconds
Instant Actual A.C.	5.32 %		Negative Press	0.12 Inches
Average Actual A.C.	5.28 %		B/H Diff. Press	2.8 Inches

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time	Temp
1	9.5	3.4	A.C.	245	245	320 Deg
2	0.0	2.5	A.C.	200	200	
3	6.6	15.7				
4	0.0	13.7				
5	0.0	2.7				
6	36.0	2.6	Mix Temp Set			320 Deg
7	28.4	4.9				
R.A.P.	14.2	7.5	4.0 A.C. %			
A.C.	5.3					
Total	100.0 %		Additive	0.00		Mix %

Lehman - Roberts


```

*****
*                               Rate   Units           Total   Units
*-----
* Production      288   Tons Per Hour      2323   Tons
* Aggregate       233   Tons Per Hour      1792.5 Tons
* Total A.C.      15.3 Tons Per Hour
* Virgin A.C.     13.7 Tons Per Hour      104.91 Tons
*
* R.A.P. A.C.     1.6 Tons Per Hour
*
* R.A.P.          40    Tons Per Hour      426.3 Tons
*
* Additive        0    Lbs Per Hour
*
*                               Agg. Composite Moisture  4.6 %
*
* Mix Temperature 340 Deg.      Sling. Position  70 %
* A.C. Temperature 322 Deg.      Burner Position  32 %
*                               Damper Position  55 %
*
* Stack Temperature 266 Deg.
*
* Instant Actual A.C. 5.33 %      B/H Pulse Time  20 Seconds
* Average Actual A.C. 5.29 %      Negative Press  0.18 Inches
*                               B/H Diff. Press  3.0 Inches
*****

```

Running Mix # 51

Name : 411-E

Description : 411-E/W RAP AC IN RAP 3.5%

```

*****
* Feeder # 1  9.5 Mix %   3.4 Moist %   A.C. On Time  245 Sec
* Feeder # 2  0.0 Mix %   2.5 Moist %   A.C. Off Time 200 Sec
* Feeder # 3  6.6 Mix %   15.7 Moist %
* Feeder # 4  0.0 Mix %   13.7 Moist %
* Feeder # 5  0.0 Mix %   2.7 Moist %
* Feeder # 6  36.0 Mix %  2.6 Moist %   Mix Temp Set  320 Deg
* Feeder # 7  28.4 Mix %  4.9 Moist %
*
* R.A.P.      14.2 Mix %   7.5 Moist %   4.0 A.C. %
*
* A.C.        5.3 Mix %
*
*-----
* Total      100.0 %
*
* Additive    0.00 Mix %
*****

```

09-30-91 17:13:42 Bin #4 High

Lehman - Roberts

09-30-91

17:14:06

```

*****
*           Rate   Units           Total   Units
*-----
* Production   291   Tons Per Hour   2375   Tons
* Aggregate    237   Tons Per Hour   1832.3 Tons
* Total A.C.   15.4 Tons Per Hour
* Virgin A.C.  13.8 Tons Per Hour   107.25 Tons
*
* R.A.P. A.C.   1.6 Tons Per Hour
*
* R.A.P.       39   Tons Per Hour   435.5 Tons
*
* Additive     0   Lbs Per Hour
*
*                               Agg. Composite Moisture  4.6 %
*
* Mix Temperature 325 Deg.   Sling. Position  70 %
* A.C. Temperature 322 Deg.   Burner Position  35 %
*                               Damper Position  55 %
*
* Stack Temperature 249 Deg.
*                               B/H Pulse Time  20 Seconds
* Instant Actual A.C. 5.29 %   Negative Press  0.16 Inches
* Average Actual A.C. 5.29 %   B/H Diff. Press  2.8 Inches
*****

```

```

*
* Running Mix # 51
* Name : 411-E
* Description : 411-E/W RAP AC IN RAP 3.5%

```

```

*****
* Feeder # 1  9.5 Mix %   3.4 Moist %   A.C. On Time 245 Sec
* Feeder # 2  0.0 Mix %   2.5 Moist %   A.C. Off Time 200 Sec
* Feeder # 3  6.6 Mix %   15.7 Moist %
* Feeder # 4  0.0 Mix %   13.7 Moist %
* Feeder # 5  0.0 Mix %   2.7 Moist %
* Feeder # 6  36.0 Mix %   2.6 Moist %   Mix Temp Set 320 Deg
* Feeder # 7  28.4 Mix %   4.9 Moist %
*
* R.A.P.      14.2 Mix %   7.5 Moist %   4.0 A.C. %
*
* A.C.        5.3 Mix %
*
*-----
* Total 100.0 %           Additive 0.00 Mix %
*
*****

```

09-30-91 17:23:14 Bin #5 High

	Rate	Units	Total	Units
* Production	308	Tons Per Hour	2426	Tons
* Aggregate	248	Tons Per Hour	1872.4	Tons
* Total A.C.	16.0	Tons Per Hour		
* Virgin A.C.	14.3	Tons Per Hour	109.61	Tons
* R.A.P. A.C.	1.7	Tons Per Hour		
* R.A.P.	42	Tons Per Hour	445.0	Tons
* Additive	0	Lbs Per Hour		
			Agg. Composite Moisture	4.6 %
* Mix Temperature	314	Deg.	Sling Position	70 %
* A.C. Temperature	322	Deg.	Burner Position	43 %
			Damper Position	55 %
* Stack Temperature	247	Deg.		
			B/H Pulse Time	20 Seconds
* Instant Actual A.C.	5.22	%	Negative Press	0.15 Inches
* Average Actual A.C.	5.28	%	B/H Diff. Press	2.7 Inches

Running Mix # 51
 Name : 411-E
 Description : 411-E/W RAP AC IN RAP 3.5%

Feeder #	Mix %	Moist %	A.C.	On Time	Off Time
* Feeder # 1	9.5	3.4	A.C.	245	245 Sec
* Feeder # 2	0.0	2.5	A.C.	Off	200 Sec
* Feeder # 3	6.6	15.7			
* Feeder # 4	0.0	13.7			
* Feeder # 5	0.0	2.7			
* Feeder # 6	36.0	2.6	Mix Temp Set	320	Deg
* Feeder # 7	28.4	4.9			
* R.A.P.	14.2	7.5	4.0 A.C. %		
* A.C.	5.3				
Total		100.0 %	Additive	0.00	Mix %

09-30-91 Lehman - Roberts 17:29:05
 Plant Status Report

	Rate	Units	Total	Units
* Production	297	Tons Per Hour	2452	Tons
* Aggregate	240	Tons Per Hour	1892.1	Tons
* Total A.C.	15.7	Tons Per Hour		

* R.A.P. A.D. 1.6 Tons Per Hour

* R.A.P. 41 Tons Per Hour 448.8 Tons

* Additive 8 Lbs Per Hour

App. Disposal Mils. 4.8 %

Mix Temperature 315 Deg. Bling. Position 70 %

A.D. Temperature 322 Deg. Burner Position 27 %

Stack Temperature 348 Deg. Damper Position 23 %

Instant Actual A.D. 5.22 % 3/4 Pulse Time 20 Seconds

Average Actual A.D. 5.17 % Negative Press 0.15 Inches

3/4 Diff. Press: 2.3 Inches

Running Mix # 31

Name : 411-E

Description : 411-E/W RAP 30 IN RAP 3.54

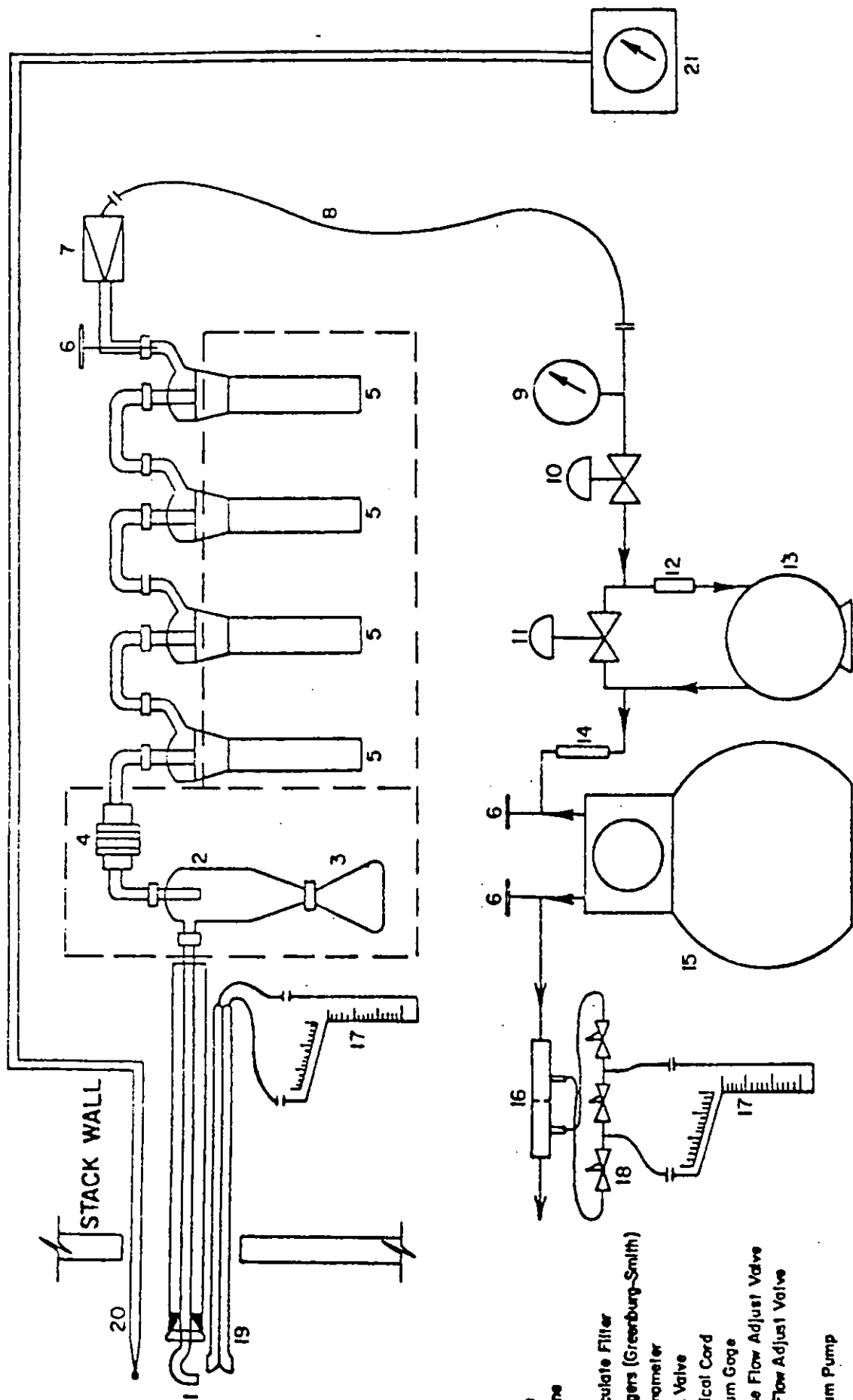
Feeder #	Mix %	Moles %	A.D.	Temp	Temp
Feeder # 1	9.8 Mix %	1.4 Moles %	A.D.	17	Temp 348 Deg
Feeder # 2	9.8 Mix %	2.3 Moles %	A.D.	277	Temp 322 Deg
Feeder # 3	9.8 Mix %	13.7 Moles %			
Feeder # 4	9.8 Mix %	11.7 Moles %			
Feeder # 5	9.8 Mix %	3.7 Moles %			
Feeder # 6	16.8 Mix %	1.6 Moles %		Mix Temp Set	312 Deg
Feeder # 7	22.1 Mix %	6.9 Moles %			
A.D.	14.2 Mix %	7.8 Moles %		A.D. A.D. %	
A.D.	5.2 Mix %				

Total 30.2 %

V. EQUIPMENT USED

Equipment used on conducting the particulate emissions test was:

- A. The Lear Siegler PM-100 stack sampler with appropriate auxillary equipment and glassware. The train was set up according to the schematic on the nex page.
- B. An Airguide Instruments Model 211-B (uncorrected) aneroid barometer was used to check the barometric pressure.
- C. Weston dial thermometers are used to check meter temperatures. An Analogic Model 2572 Digital Thermocouple is used for stack temperatures.
- D. A Hays 621 Analyzer was used to measure the oxygen, carbon dioxide and carbon monoxide content of the stack gases. For non-combustion sources, A Bacharach Instrument Company Fyrite is used for the gas analysis.
- E. Filters are mady by Schleicher and Schuell and are type 1-HV with a porosity of .03 microns.
- F. The acetone is reagent grade or ACS grade with a residue of \leq .001.



SAMPLING TRAIN USED FOR ISOKINETIC SAMPLING

- 1) Probe
- 2) Cyclone
- 3) Flask
- 4) Particulate Filter
- 5) Impingers (Greenburg-Smith)
- 6) Thermometer
- 7) Check Valve
- 8) Umbilical Cord
- 9) Vacuum Gage
- 10) Course Flow Adjust Valve
- 11) Fine Flow Adjust Valve
- 12) Orifer
- 13) Vacuum Pump
- 14) Filter
- 15) Dry Gas Meter
- 16) Orifice Tube
- 17) Incline Manometer
- 18) Solenoid Valves
- 19) Pilot
- 20) Thermocouple
- 21) Pyrometer

8610 Gas Chromatograph

Miniature Lab GC

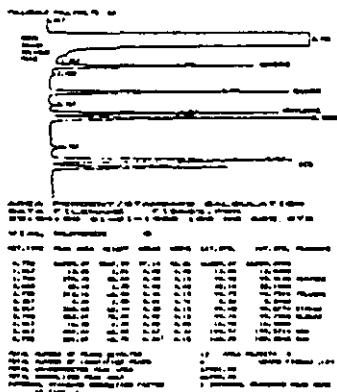
At a fraction of the cost, the SRI 8610 Gas Chromatograph provides the capabilities and sophistication of vastly larger and more expensive instruments in a small, lightweight and attractive package. More of a miniaturized laboratory GC than a true portable, the 8610 is the perfect size and weight for easy field use without sacrificing big GC features. In the lab or in the field, the 8610 Gas Chromatograph gives you up to five detectors plus a built-in purge and trap in a simple to operate, easy to troubleshoot, and unbelievably low cost package. And, the Peaksimple Data System, provided free with every 8610 GC turns your IBM PC into a powerful chromatography integrator which also controls the 8610's temperature program and purge and trap.

Multi-Level Temperature Programming

Temperature programming is a standard feature on every 8610 GC. Up to 15 ramp/plateau segments permit maximum flexibility. Because the temperature program is controlled by the data system, an unlimited number of different temperature programs may be permanently stored on disk and activated with a few keystrokes. The 8610's temperature program can be controlled either by the Peaksimple Data System (included free with every GC) or by any other data system or integrator which has the ability to close relay contacts at specified times during the run.

Ultra Low Mass Column Oven

The SRI 8610's large easily accessible column oven is designed to fit all standard packed and capillary columns with diameters up to eight inches. The ultra-low mass design allows rapid heat-up and cool-down from ambient to 250 degrees centigrade. Interchangeable screw-in heater elements allow power consumption to be reduced for low temperature battery powered applications, or easy heater replacement in the event of a failure. Squirrel-cage type oven fan insures uniform heat distribution and stability to within .1 degree.



100 NG.
602 STD.
Data
plotted
using
Peaksimple
Data
System.

Low Cost GC • Free Data System/Integrator
Field Portable • Built-In Purge and Trap
Temperature Programmable • Multiple Detectors

Digital Gas Flow Controllers

The carrier gas flow rate is regulated by a unique Digital Flow Controller. Precise and reproducible even at capillary flow rates below 1 cc/per minute, the carrier gas flow controller is standard equipment on every SRI 8610 GC (except low-cost student model). Digital dial allows flow rates to be adjusted without having to measure actual flows with a bubblemeter. A column head pressure gauge is provided to alert the operator to leaks or blockages in the column. The same flow controller is optionally available for hydrogen and air combustion gas flows (recommended for NPD operation). In addition, inlet pressure regulators are supplied for each gas to isolate the GC from fluctuations in gas supply pressure.

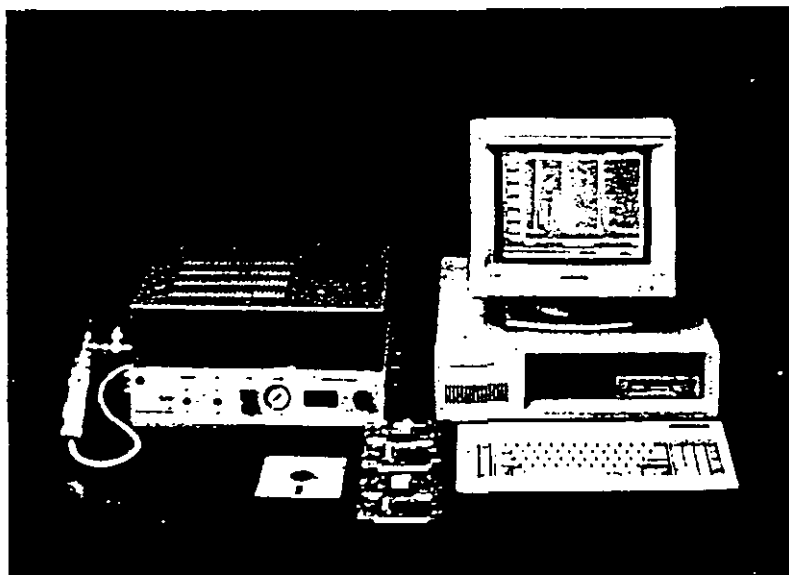
Direct Cool On Column Injection

The zero-dead volume on-column injector is designed for state of the art, cool on-column injections using both packed and wide-bore capillary (.53mm.). A special wide-bore adapter positions the .53mm column so the syringe smoothly deposits the sample in the bore of the column itself. This provides a totally inert, metal and glass free sample path. Peaks are exceptionally sharp and well resolved.

Detectors

Thermal Conductivity (TCD)	Photo-Ionization (PID)
Flame Ionization (FID)	Electron Capture (ECD)
Nitrogen-Phosphorus (NPD)	Hall Detector (HALL or ELCD)
Thermionic Ionization (TID)	Flame Photometric (FPD)

Up to 3 detectors may be mounted simultaneously and plumbed in series so that one injection passes through each detector and into the next. Common series configurations include: (PID-FID), (TCD-FID), (PID-ECD), (PID-HALL) and (PID-ECD-FID).



PRINCIPLES OF OPERATION

Servomex

1400 Series Gas Analyzers

SPECIFICATION

OXYGEN

Principle	Magneto-dynamic
Linearity	$\pm 0.2\% \text{ O}_2$
Repeatability	$\pm 0.2\% \text{ O}_2$
Zero Drift (Per Week)	$< 0.2\% \text{ O}_2$
Signal Output	0-1V non-isolated for 0-100% O_2

Alarms	Flow alarm. 4 sets of changeover relay contacts rated at 3A/120V AC, 1A/240V AC or 1A/28V DC
--------	--

Display	3½ digit LCD reading 0 to 100% O_2
---------	---

Response Time	Less than 15 seconds to 90%
---------------	-----------------------------

Operating Ambient Temperature	32 - 104°F (0 - 40°C)
-------------------------------	-----------------------

Relative Humidity	0 - 85%, non-condensing
-------------------	-------------------------

Sample Pressure	0.2 to 0.6 barg
-----------------	-----------------

Flowrate	1.5 to 6 liters/min
----------	---------------------

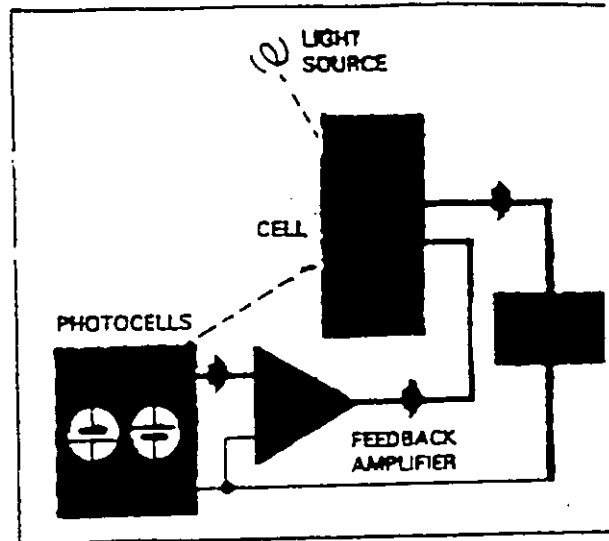
Sample Condition	Clean, dry, non-toxic, non-flammable gas
------------------	--

Sample Contact Materials	Stainless steel, pyrex glass, brass, platinum, epoxy resin, viton, polypropylene and glass fibre
--------------------------	--

AC Supply	110 to 120V AC, or 220 to 240V AC, $\pm 10\%$, 48 to 62Hz, 15VA maximum
-----------	--

Dimensions	19" Rack - 4U case Bench top - 7.1" (180mm) high, 10.1" (256mm) wide, 15.4" (390mm) deep
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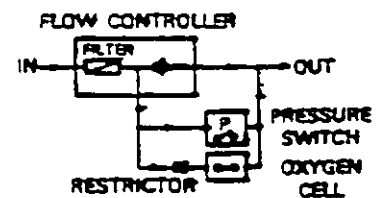
22 lbs (10kg) approximately



PARAMAGNETIC OXYGEN

The oxygen analyzer measures the paramagnetic susceptibility of the sample gas by means of a magneto-dynamic type measuring cell.

Oxygen is virtually unique in being a paramagnetic gas, this means that it is attracted into a magnetic field. In the Servomex measuring cell, the oxygen concentration is detected by means of a dumb-bell mounted on a torque suspension in a strong, non-linear magnetic field. The higher the concentration of oxygen, the greater the dumb-bell is deflected from its rest position. This deflection is detected by an optical system and twin photocells connected to an amplifier. Around the dumb-bell is a coil of wire. A current is passed through this coil to return the dumb-bell to its original position. The current is measured and is proportional to the oxygen concentration.



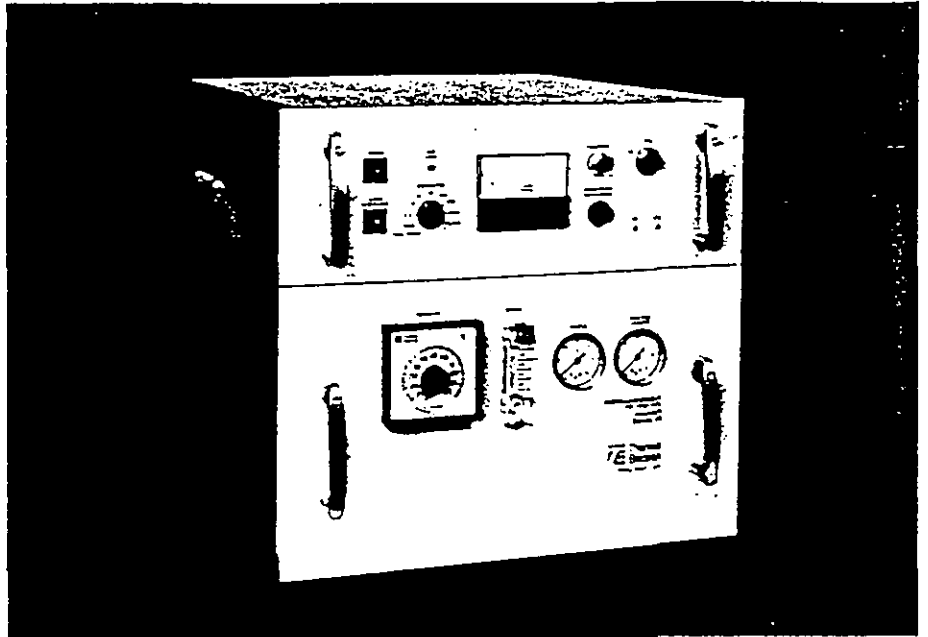
Gas Flow Diagram

Advantages

- Not cross-sensitive to most common gases
- Long lifetime
- Rugged design
- No routine cell maintenance

Chemiluminescent NO/NO_x Analyzer

Model 10 For Continuous Source Gas Monitoring



Thermo Electron's Model 10 NO/NO_x Analyzer is based on the chemiluminescent reaction between nitric oxide (NO) and ozone (O₃) according to the reaction:



Light emission results when the electronically excited NO₂ molecules revert to their ground state.

A front panel mode switch provides for either a direct readout of the NO concentration in the sample being analyzed ("NO" mode) or the total NO_x concentration ("NO_x" mode). When the Model 10 is placed in the "NO_x" mode, the sample stream passes through a NO_x-to-NO converter prior to entering the reaction chamber for subsequent analysis.

Key Features

- Selective detection of NO or NO_x
- Eight ranges, from 2.5 to 10,000 ppm FS
- Continuous monitoring with rapid response
- Linear on all ranges
- Field proven reliability
- Insensitive to changes in sample flow

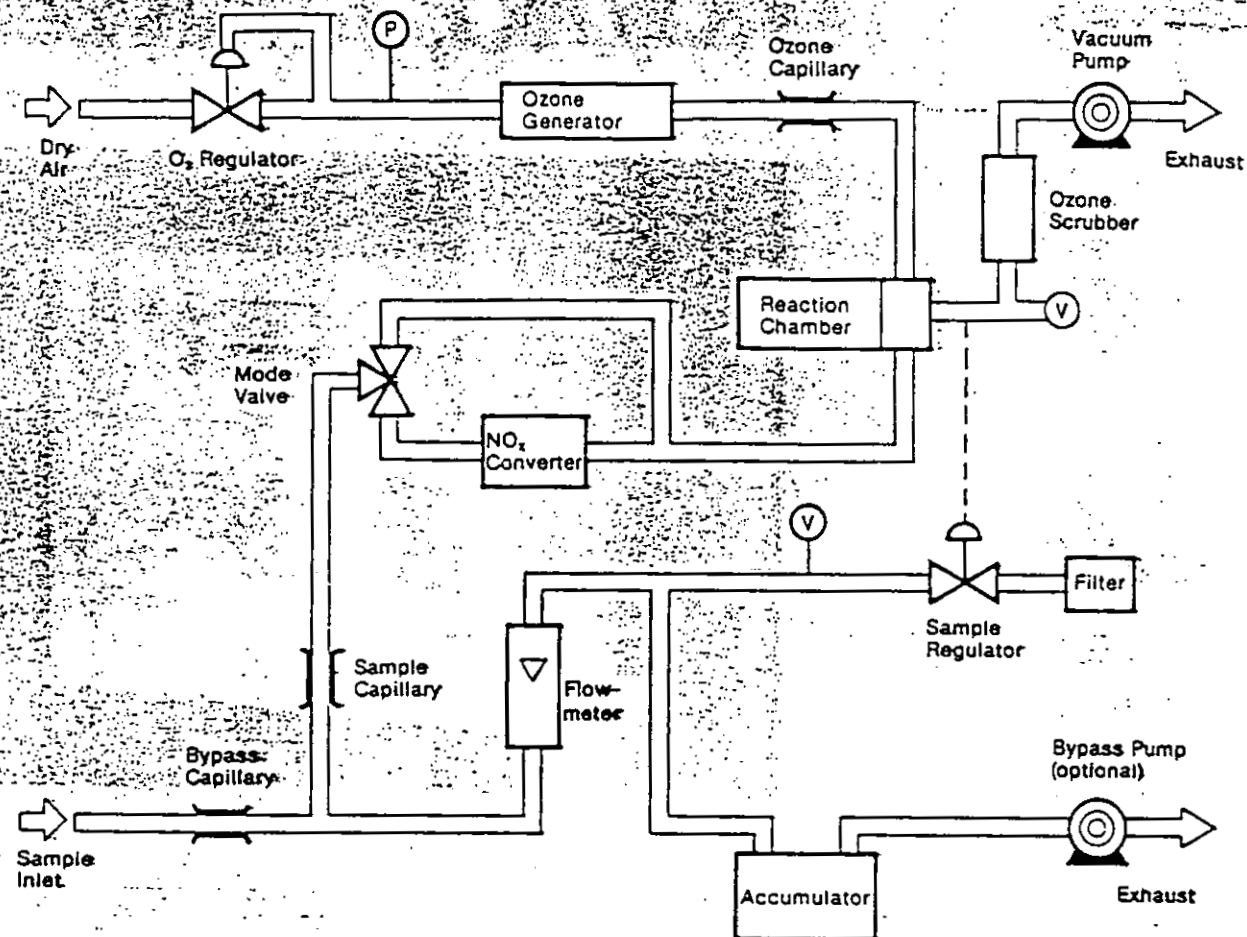
Model 10 Specifications*

Ranges	0-2.5 ppm 0-10 ppm 0-25 ppm 0-100 ppm	0-250 ppm 0-1000 ppm 0-2500 ppm 0-10,000 ppm
Minimum Detectable Concentration	.05 ppm	
Noise	Less than 1% of FS	
Reproducibility	1% of FS	
Operating Temperature Extremes	0-40°C	
Response Time (0-90%)	~ 1.5 second NO mode ~ 1.7 second NO _x mode	
Zero Stability	± 1 ppm in 24 hours	
Span Stability	± 1% in 24 hours	
Linearity	± 1% from 0.05 to 10,000 ppm**	
Power Requirements	1000 watts, 115 ± 10 volts, 60 Hz standard. Also available in 115V 50 Hz, and 210 ± 15 volts, 50 Hz versions	
Physical Dimensions	19" wide × 17" high × 20" deep	
Instrument Weight	75 lbs. (including pump)	
Outputs	Two standard outputs supplied: 1) 0-10V; 2) Field selectable from 0-10V, 5V, 1V, 100mV or 10mV. (ma options available.)	

*Specifications are typical and subject to change without notice.

**With O₃ Feed; With dry air, linearity to 2000 ppm.

Model 10 Flow Scheme



As illustrated in the above diagram, sample gas enters the Model 10, flows through the bypass capillary, and divides. Most of the sample flows through the flowmeter, accumulator, bypass pump, and exhausts. Only a small amount of sample flows through the sample capillary for analysis. The bypass pump in conjunction with the sample regulator maintain a constant pressure differential across the sample capillary, thus maintaining constant sample flow for analysis. This plumbing network makes the analyzer insensitive to pressure fluctuation in the sample inlet.

From the sample capillary, the sample to be analyzed is either directed through the NO_x to NO converter or around it, depending on the choice of the operator. In the reaction chamber the sample reacts with ozone to produce the light emission and is exhausted. The ozone is produced internally from dry air entering through the oxygen regulator and ozonator. The light emission is sensed by the photomultiplier tube and amplified.

Options

10-001 Bypass pump assembly includes pump, snock tray, accumulator, tubing, and fittings.

Accessory Instruments

Model 700 Heated Capillary Module
 Model 606H Heated Particulate Filter
 Model 800 Sample Gas Conditioner
 Model 900 Sample Gas Conditioner

**Thermo
 Electron**
 CORPORATION

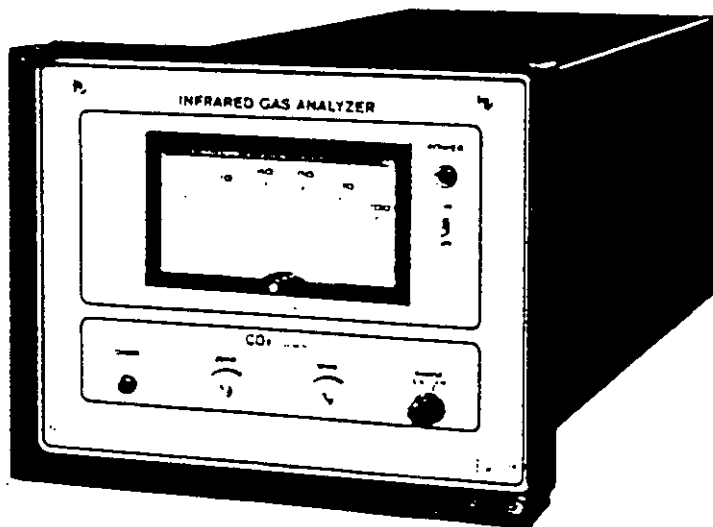
Environmental Instruments Division

108 South Street
 Hopkinton, MA 01748
 Telephone (617) 435-5321
 Telex 948325

Environmental Products

FUJI 730

NDIR SINGLE GAS ANALYZER



Analog Display Shown,
Digital Display Available

- Unique Mass Flow Sensor System Eliminates Interference
- Ideal For Applications In
 - Combustion Monitoring/Control
 - Hydrocarbon Monitoring
- Measures In Two Ranges
 - Carbon Monoxide (CO)
 - Carbon Dioxide (CO₂)
 - Methane (CH₄)
- Designed For Continuous Operation and Low Maintenance

The unique Mass Flow Sensor used in the Fuji 730 Single Gas Analyzer provides significant advantages over other sensors used for this purpose. The design of the Mass Flow Detector minimizes the adverse effects of vibration which is often present in harsh environments. In addition, the Mass Flow Sensor System virtually eliminates interference making the Fuji 730 a powerful analytical tool for monitoring burner and boiler efficiency, heat treatment, fermentation, well logging and many other applications which require exceptional accuracy, stability, high sensitivity and reliability.

See specifications on reverse side

FUJI 730 SINGLE GAS ANALYZER

SPECIFICATIONS

PRINCIPLE OF OPERATION

The Fuji 730 Series Analyzers use the infrared absorption characteristic of gases to measure the concentration of gas samples. An efficient single beam design which incorporates a unique mass flow sensor system insures accurate and interference free analysis for a wide variety of applications.

A single beam of infrared energy is chopped and passed through a sample cell containing the flowing gas sample. Due to the absorption characteristic, the amount of energy in the beam is reduced by the concentration of the measured gas in the sample. The attenuated infrared beam is passed serially through the two cavities of the mass flow sensor which contain a high concentration of the gas species the analyzer is intended to measure. The two cavity sensor performs two functions in the analyzing process, it first eliminates interference caused by other gases and water vapor by detecting and subtracting the interference component from the detector output, and secondly, produces an output signal which represents an accurate duplication of the relative infrared energy absorption. This resultant signal is electronically processed and linearized to provide an electrical signal which drives meters and other output devices.

STANDARD GASES

Carbon Monoxide (CO)
Carbon Dioxide (CO₂)
Methane (CH₄)

STANDARD RANGES

0 - 500/1000 ppm
0 - 1000/2000 ppm
0 - 2000/5000 ppm
0 - 2500/5000 ppm

0-0.5/1.0%
0-1/2%
0-2/5%
0-5/10%
1-10/20%

PURGE GAS FITTING

Standard Equipment

INTERNAL SPAN CHECK FEATURE

Calibration check without the use of span gases.
Conserves gas and reduces operating costs.

Repeatability

±0.5% of full scale (low range)
±1.0% of full scale (high range)

Zero Drift*

±1% of full scale per 24 hours

Span Drift*

±1% of full scale per 24 hours

Linearity

±2% of full scale (with linearizer)

Noise Level

0.5% of full scale

Speed of Response

90% indication

Electrical

2.3 or 5 seconds (field selectable)

Pneumatic

less than 15 seconds (depending on cell length)

Warm-Up

Two hours (to ±2% full scale)

Internal Span Check

Manually activated from front panel

Outputs

0 to 1V DC, linear & ±20mA DC, linear

Ambient Temperature Range

23 to 113°F (-5 to 45°C)

Ambient Humidity

To 90% R.H. (non-condensing)

Sample Gas Temperature

32 to 122°F (0 to 50°C)

Sample Gas Flow Rate

2 ± 1 scfh (1.0 ± 0.5 slpm)

Purge Gas Rate (where necessary)

2 scfh (1 slpm) when required

Power Requirements

115V AC ± 10%, 60 Hz, 30VA

Gas Connections

All 1/4" compression-type tube fittings

Size and Weight

7.9 (H) x 9.8 (W) x 21.3 (D) inches
(200 x 250 x 541 mm)
24.2 pounds (11 kg)

*constant conditions

Environmental Products

PACE ENVIRONMENTAL PRODUCTS

A DIVISION OF PACE ASSOCIATES, INC.

1196 EASTON ROAD

HORSHAM, PA 19044

PHONE: (215) 957-1144

FAX: (215) 957-1186

FUJI 760

NDIR GAS ANALYZER

INFRARED GAS ANALYZER



Bench Top or Rack Mount
Available

- Unique Mass Flow Sensor System Eliminates Interference
- Wide Dynamic Range Permits Ultra-Sensitive and High Concentration Gas Analysis
- Measures
 - Carbon Monoxide (CO)
 - Carbon Dioxide (CO₂)
 - Sulfur Dioxide (SO₂)
 - Nitric Oxide (NO)
 - Methane (CH₄)
- Designed For Continuous Operation and Low Maintenance
- Insensitive to Vibration

This instrument is designed for stack monitoring and process control applications. Its remarkable accuracy and fast response makes it an ideal instrument for CEMS, boiler control equipment, research labs and many other monitoring applications. For usage requiring ultra sensitive measurement, the Fuji 760 delivers superior performance. Using the Non-Dispersive Infrared (NDIR) Mass Flow Detector, low concentration measurements are accurate and reliable. The Fuji 760 incorporates an Interference Compensating Detector which minimizes the effects of other gases, particularly when operating in ranges of high sensitivity.

Warranty

Whittaker warrants each new gas analyzer of its manufacture to be free of defects in material and workmanship for one year from the date of delivery. For full warranty information, contact your representative.

See specifications on reverse side

FUJI 760 Gas Analyzer

FEATURES OF THE FUJI-760

The Fuji 760 Analyzer uses infrared absorption techniques to measure gas concentrations, however, many innovative patented features make this instrument far superior to conventional Non Dispersive Infrared Analyzers. Among its unique features are an optical chopper design which virtually eliminates the effects of vibration and resultant optical noise; a mass flow sensor system which reduces the effects of interfering gases to insignificant levels, thus permitting gas analysis at low concentration ranges; and a dual beam optical system derived from a single infrared source which enhances long term stability.

PRINCIPLE OF OPERATION

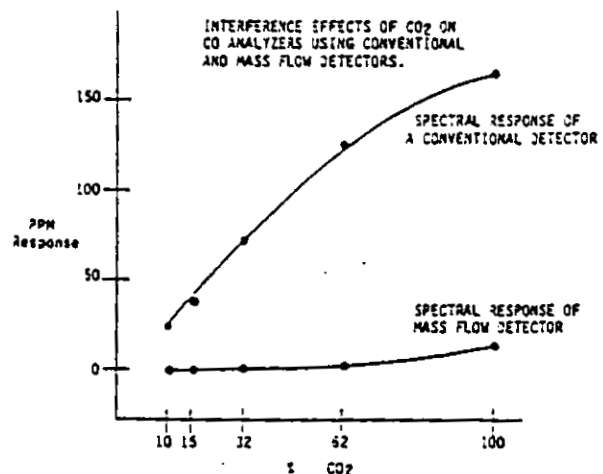
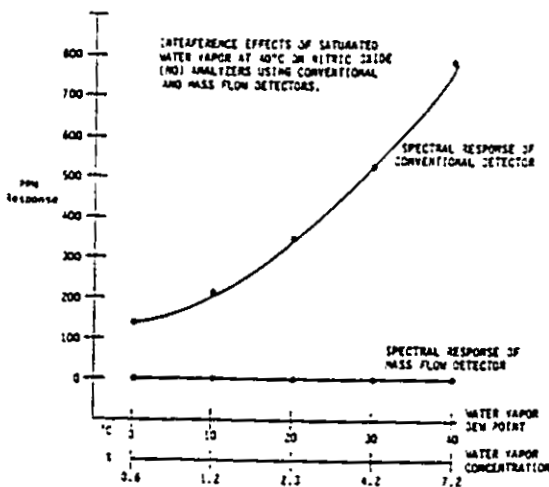
A single beam of infrared energy is modulated and split into two parallel beams by a distribution cell. One beam is passed through a reference cell containing a non-absorbing gas, and the other beam is passed through a cell containing the sample gas being measured. The beam passing through the sample cell is attenuated by the amount of gas concentration in the sample and compared against the unattenuated reference beam by the mass flow detector system. One set of detectors sense the amount of sample gas as compared against the reference, the second set of detectors measure and cancel interferences in the sample. The outputs of the detectors are electronically processed and conditioned into useable signals for indicators and other output devices.

Detectable Gas Ranges

Standard Configuration

Component	Minimum Range
Carbon Monoxide (CO)	0 to 100 ppm
Carbon Dioxide (CO ₂)	0 to 50 ppm
Nitric Oxide (NO)	0 to 100 ppm
Sulfur Dioxide (SO ₂)	0 to 100 ppm
Total Hydrocarbons	0 to 500 ppm

Other Gases can be measured. Call our applications engineer or your local sales representative to discuss the suitability for your specific needs.



Specifications (Standard Configuration)

- Repeatability**
± 0.5% of full scale
- Zero Drift**
± 2% of full scale per week
- Span Drift**
± 2% of full scale per week
- Linearity**
± 2% of full scale
- Speed of Response**
90% indication within 5 seconds (Electronic Response)
- Range Selection**
Either of two ranges selected by front panel switch or external contact closure.
- Warm-Up**
Four hours minimum
- Outputs**
0 to 1V DC, linear and 4-20mA DC, linear
- Ambient Temperature Range**
23 to 113°F (-5 to 45°C)
- Ambient Humidity**
To 90% R.H. (non-condensing)
- Sample Gas Temperature**
32 to 122°F (0 to 50°C)
- Sample Gas Flow Rate**
1.0 ± 0.5 scfh (0.50 ± 0.25 slpm) for standard configuration
- Materials in Contact with Sample**
304 stainless steel, neoprene rubber, rubber, CaF₂ sapphire, Teflon®
- Power Requirements**
115V AC ± 10%, 50/60 Hz (switch selectable)
110 VA max. (200VA max with converter).
220V AC available
- Gas Connections**
All 1/4 inch compression-type tube fittings
- Size and Weight**
3.66 (H) x 17.44 (W) x 16.78 (D) inches
(220 x 443 x 350 mm).
37.4 pounds (17 kg).



PACE ENVIRONMENTAL PRODUCTS

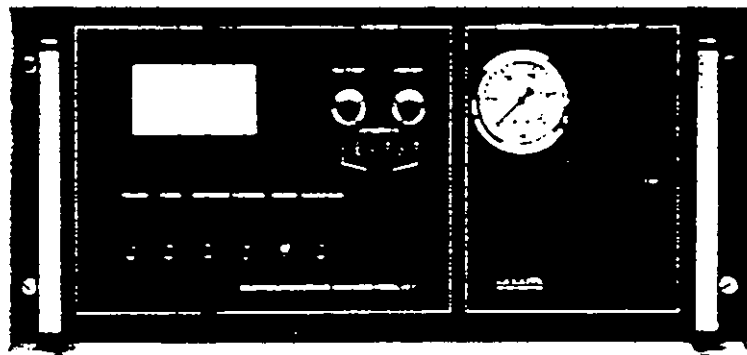
A DIVISION OF PACE ASSOCIATES, INC.

1196 EASTON ROAD
HORSHAM, PA 19044

PHONE: (215) 957-1144



HEATED TOTAL HYDROCARBON ANALYZER MODEL VE7



The J.U.M. Engineering Model VE7 is a high accuracy Total Hydrocarbon Analyzer for the measurement and analysis of organic vapors.

The VE 7 utilizes a Hydrogen Flame Ionization Detector (FID) in a thermostatically controlled oven to prevent the loss of high molecular weight hydrocarbons.

Options

Digital display with BCD output/without BCD output
Remote range control and range I.D.
Recorder output of oven temperature

- All heated components
- Integrated heated sample pump
- Permanent heated stainless steel 2 micron sample filter
- Built in burner air supply- no extra bottles needed
- Automatic fuel enrichment for ignition
- 19 inch relay rack mount
- 1% precision full scale
- Response time- 90% full scale within 1 second

STANDARD SPECIFICATIONS:

Analysis Method:
Sensitivity:
Response Time:
Zero Drift:
Span Drift:
Linearity:
Oxygen Synergism:
Ranges:

Outputs:
Display:
Zero/Span Adjust:
Fuel Consumption:

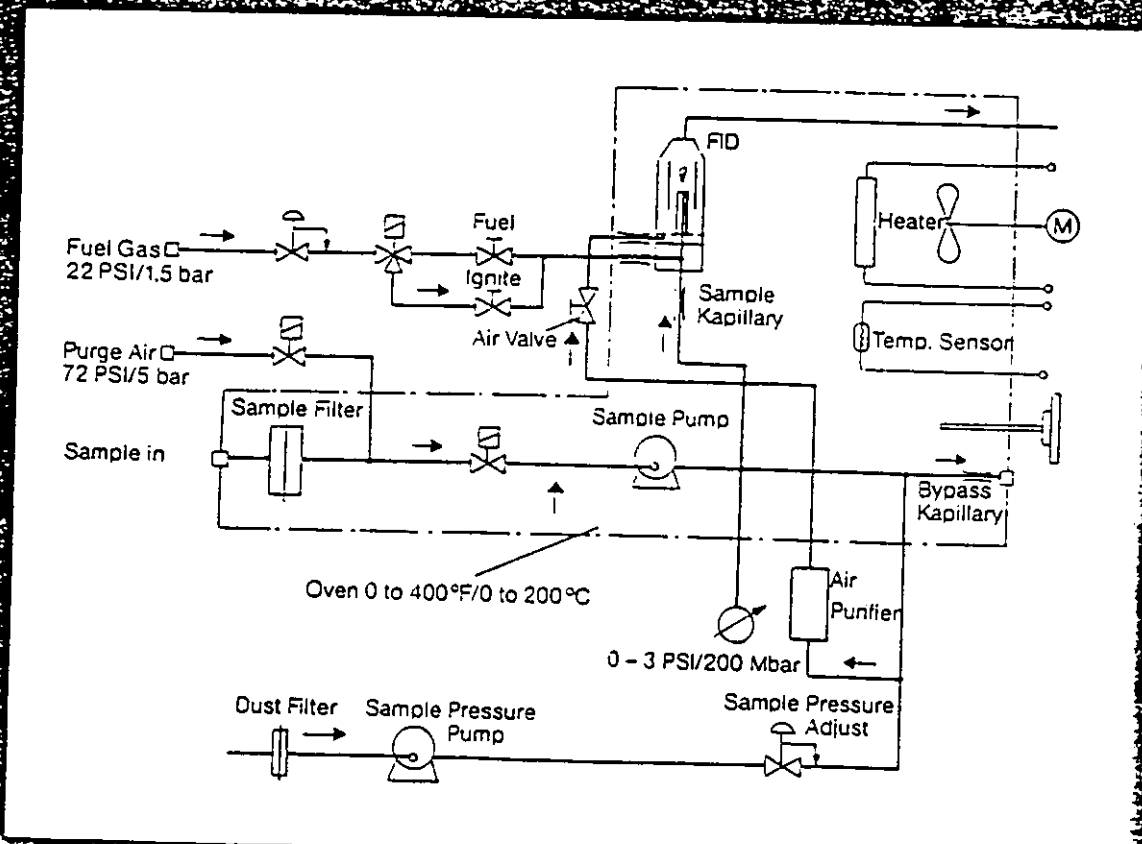
Air Consumption:
Zero & Span Gas:
Sample Pump:

Sample Pressure:
Sample Filter:

Analysis Temperature:
Power Requirements:
Ambient Temperature:
Dimensions:

Weight:
Shipping Weight:

Flame Ionization Detector (FID)
Max. 1 ppm CH₄
90% of full scale in less than one second
1% of full scale per 24 hours
1% of full scale per 24 hours
Within 1%
Less than 1% of selected range
Any three of the following:
0-10, 100, 1000, 10,000, 100,000 ppm
0-10 Volts D.C.
Analog Meter in ppm Hydrocarbon or in % LEL
Manual on front panel
Hydrogen 20 cc/min at 22 psig (1.5 Bar)
Hydrogen/Helium 40/60 mix 80 cc/min
None, Integral Air generator
3 psig (200 m Bar)
All Stainless Steel, heated, 3 liters per minute at
operating temperature
By Integral Pump 3 psig (200 m Bar)
Permanent all stainless steel, 2 micron back
purged for cleaning
Adjustable 200 to 400°F (93 to 204°C)
110 Volts 60 Herz AC, 800 Watts (others on request)
32°F to 110°F (0 to 43°C)
Width 483 mm (19 inches)
Depth 460 mm (18 1/8 inches)
Height 227 mm (8 3/4 inches)
38.6 lbs. (17.5 kg)
53 lbs. (24 kg)



VI. LABORATORY ANALYSIS
A. PAH ANALYSIS

TRIANGLE LABORATORIES, INC.

801 Capitola Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE815
 RF FILE: FE807
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/19/91

SAMPLE ID: RUN #1
 DILN FACTOR: 1
 TLI Sample ID: 46.060.1A.H

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	1456		309	1		IS	
Naphthalene-d8	8130		483	14		IS	
Naphthalene	44684	.9104	487	14	320.28	D	10
2-Methylnaphthalene	17973	.7186	589	14	163.20	D	10
Acenaphthene-d10	5247		736	28		IS	
2-Chloronaphthalene	0	.9327	0	28	.16	ND	10
Acenaphthylene	19639	1.5120	714	28	99.02	D	10
Acenaphthene	0	1.0072	0	28	.15	ND	10
Fluorene	5565	.9405	816	28	45.11	D	10
Phenanthrene-d10	11012		950	47		IS	
Phenanthrene	7446	1.0774	953	47	25.10	D	10
Anthracene	940	1.0176	960	47	3.36	E	10
Fluoranthene	755	1.1700	1123	47	2.34	E	10
Chrysene-d12	9089		1338	57		IS	
Pyrene	813	.9377	1154	57	3.82	E	10
Benzo(a)anthracene	0	1.0234	0	57	.09	ND	10
Chrysene	0	1.0396	0	57	.08	ND	10
Perylene-d12	9237		1557	64		IS	
Benzo(b)fluoranthene	0	.8831	0	64	.10	ND	10
Benzo(k)fluoranthene	0	.9783	0	64	.09	ND	10
Benzo(e)pyrene	0	.8487	0	64	.10	ND	10
Benzo(a)pyrene	0	.9448	0	64	.09	ND	10
Perylene	0	.5627	0	64	.15	ND	10
Indeno(1,2,3-cd)pyrene	0	.8595	0	64	.10	ND	10
Dibenz(a,h)anthracene	0	.9225	0	64	.09	ND	10
Benzo(g,h,i)perylene	0	.9620	0	64	.09	ND	10

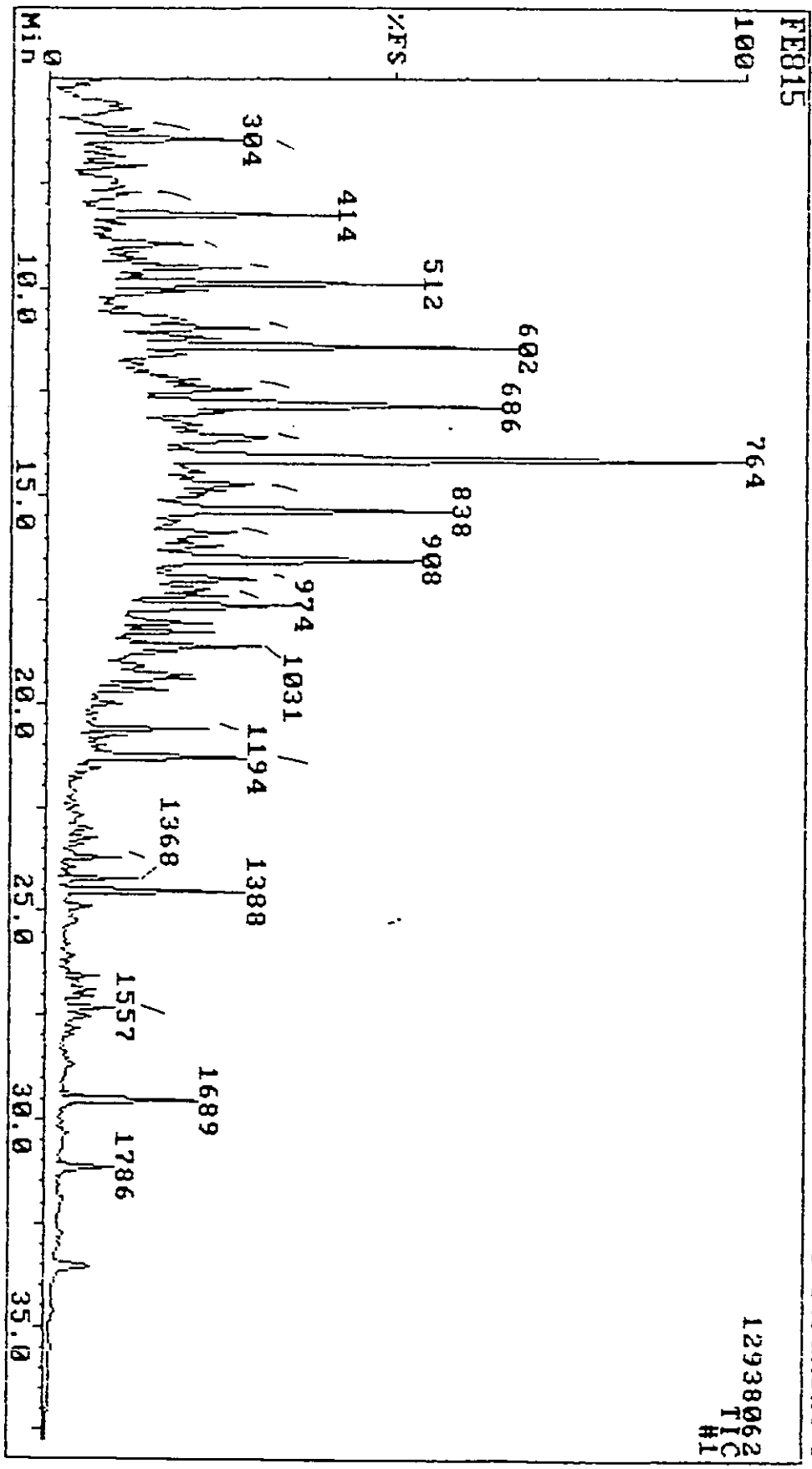
SURROGATE	SUMMARY	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14		19703	.6288	1195	57	137.90	D	137.9
Anthracene-d10		18508	.9242	958	47	72.74	D	72.7
Pyrene-d10		20384	.6547	1152	57	137.02	D	137.0
Phenol-d5		3210	1.1959	281	1	73.73	D	73.7
2,4,6-Tribromophenol		2039	.0779	852	28	199.50	D	199.5
1,4-Dibromobenzene-d4		1800	.4698	492	1	105.27	D	105.3

CODES: ND = Not Detected; D = Detected; E = Estimated; IS = Internal Standard

19-Sep-91 18:36
Sample: RUN#1 18976

Triangle Labs, Inc.

(919) 544-5729
Instrument F



Smj

N	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	49	33	87	5	145630	bb	309	152 1,4 Dichlorobenzene-d4
2	45	23	77	-4	612980	vv	483	136 Naphthalene-d8
3	92	74	97	2	4468400	bv	467	128 Naphthalene
4	83	54	89	1	1797300	vv	589	142 2-Methylnaphthalene
5	64	24	79	0	524690	bv	736	164 Acenaphthene-d10
6	0	0	0	0	0		0	162 2-Chloronaphthalene
7	88	44	97	0	1963900	vv	714	152 Acenaphthylene
8	0	0	0	0	0		0	153 Acenaphthene
9	70	31	81	0	556540	vv	816	166 Fluorene
10	76	31	91	0	1101200	vv	950	188 Phenanthrene-d10
11	74	26	93	0	744640	vv	953	178 Phenanthrene
12	51	11	76	-1	94013	vv	960	178 Anthracene
13	41	15	77	-4	75497	vv	1123	202 Fluoranthene
14	57	64	94	-6	908920	vb	1338	240 Chrysene-d12
15	85	61	98	2	1970300	vb	1195	244 Terphenyl-d14
16	50	13	80	2	81330	bv	1154	202 Pyrene
17	0	0	0	0	0		0	228 Benzo(a)anthracene
18	0	0	0	0	0		0	228 Chrysene
19	89	61	93	1	923710	bb	1557	264 Perylene-d12
20	0	0	0	0	0		0	252 Benzo(b)fluoranthene
21	0	0	0	0	0		0	252 Benzo(k)fluoranthene
22	0	0	0	0	0		0	252 Benzo(e)pyrene
23	0	0	0	0	0		0	252 Benzo(a)pyrene
24	0	0	0	0	0		0	252 Perylene
25	0	0	0	0	0		0	276 Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0		0	278 Dibenz(a,h)anthracene
27	0	0	0	0	0		0	276 Benzo(g,h,i)perylene
28	0	0	0	0	0		0	266 Pentachlorophenol
29	66	38	85	2	368940	bv	386	82 Nitrobenzene-d5
30	64	36	75	-1	864220	bv	648	172 2-Fluorobiphenyl
31	64	21	82	0	203860	bb	852	330 2,4,6-Tribromophenol
32	61	37	86	3	321030	bb	281	99 Phenol-d5
33	79	63	97	3	2038400	vv	1152	212 Pyrene-d10
34	91	49	96	0	1850800	vv	958	188 Anthracene-d10
35	52	18	87	-3	180050	bb	492	240 1,4-Dibromobenzene-d4
36	62	30	76	1	234520	bb	433	185 1,3,5-Trichlorobenzene-d3

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Sample: RUN#1 18976

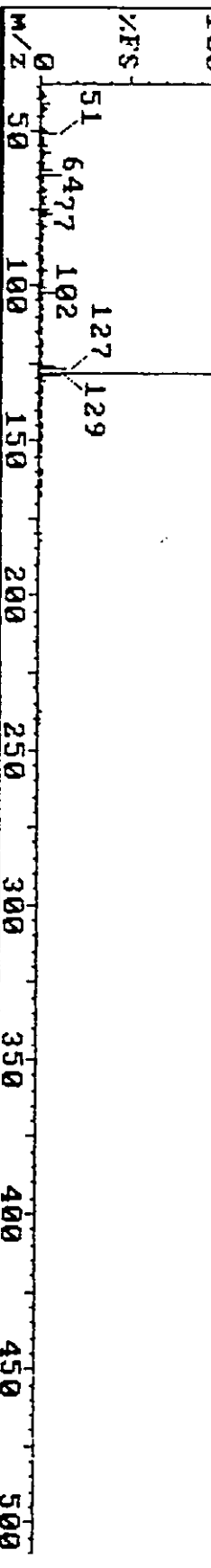
Triangle Labs, Inc.

(919) 544-5729
Instrument F

FEB15 487 (9.517)

100 128

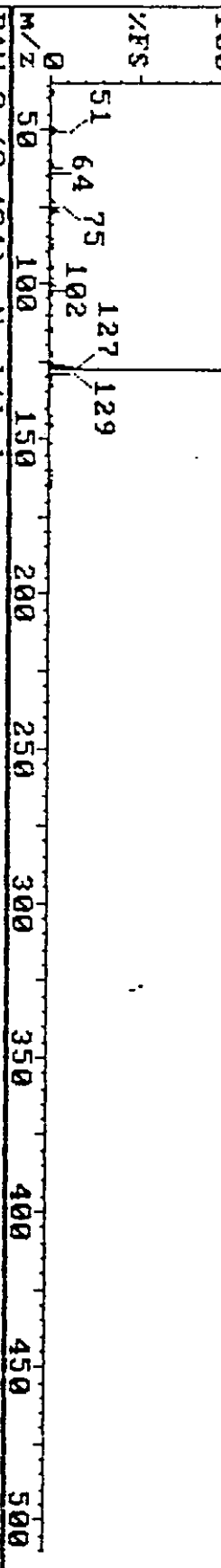
1196032



FEB15 487 (9.517) REFINE

100 128

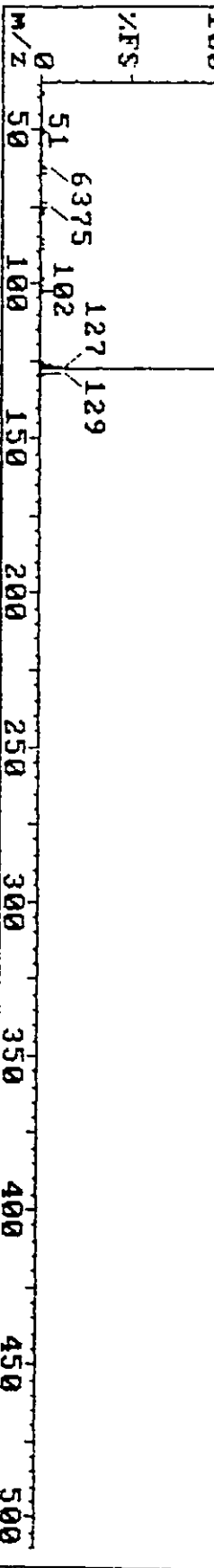
1179648



PAH 3 (9.434) Naphthalene

100 128

FIND 100



19-Sep-91 18:36

Triangle Labs, Inc.

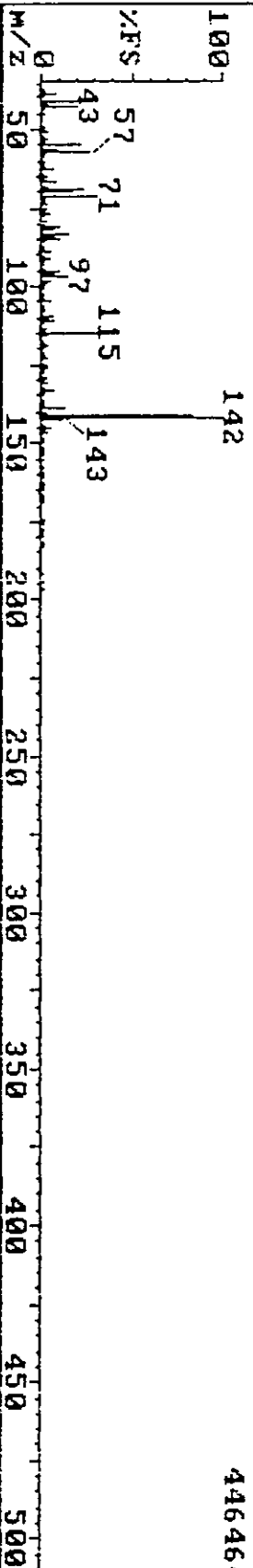
(919) 544-5729

Sample: RUN#1 18976

Instrument F

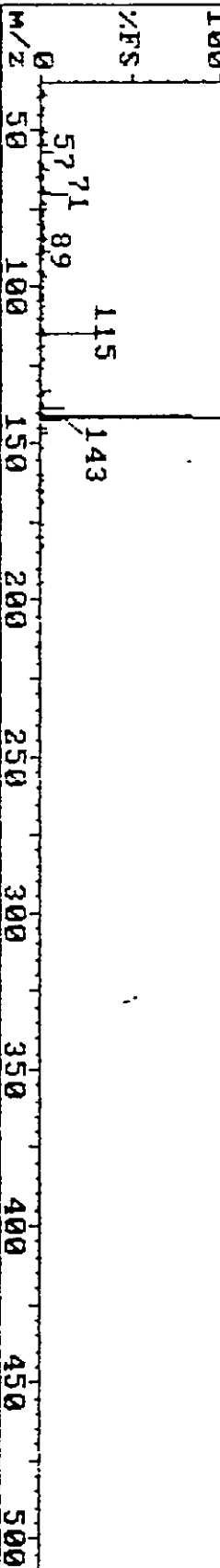
FE815 589 (11.217)

446464



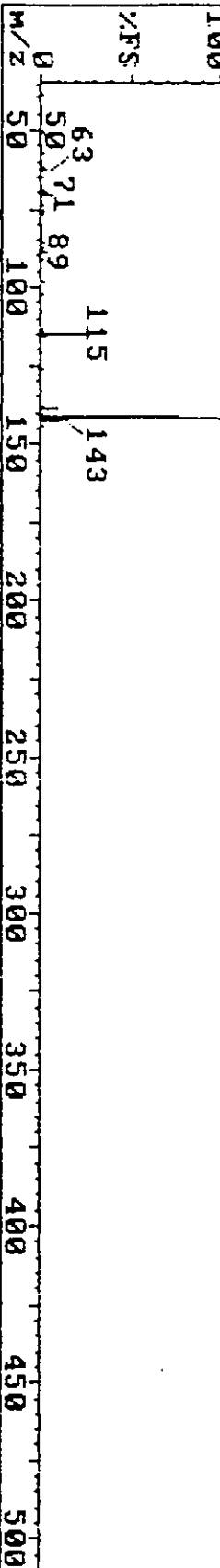
FE815 589 (11.217) REFINE

430080



PAH 4 (11.134) 2-Methylnaphthalene

FIND



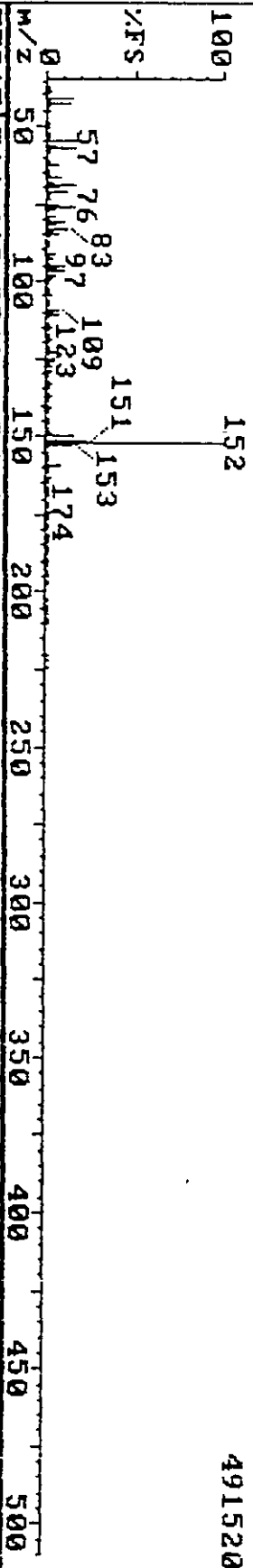
19-Sep-91 18:36

Sample: RUN#1 18976

Triangle Labs, Inc.

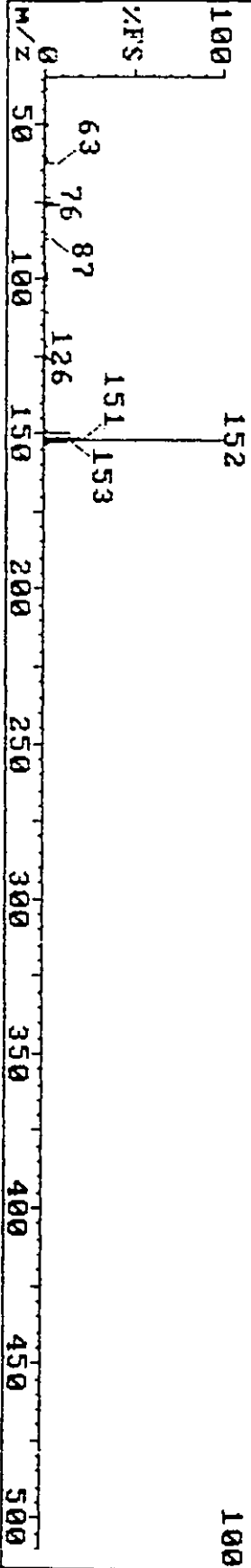
(919) 544-5729
Instrument F

FEB15 714 (13.301)



466944

PAH 7 (13.234) Acenaphthylene

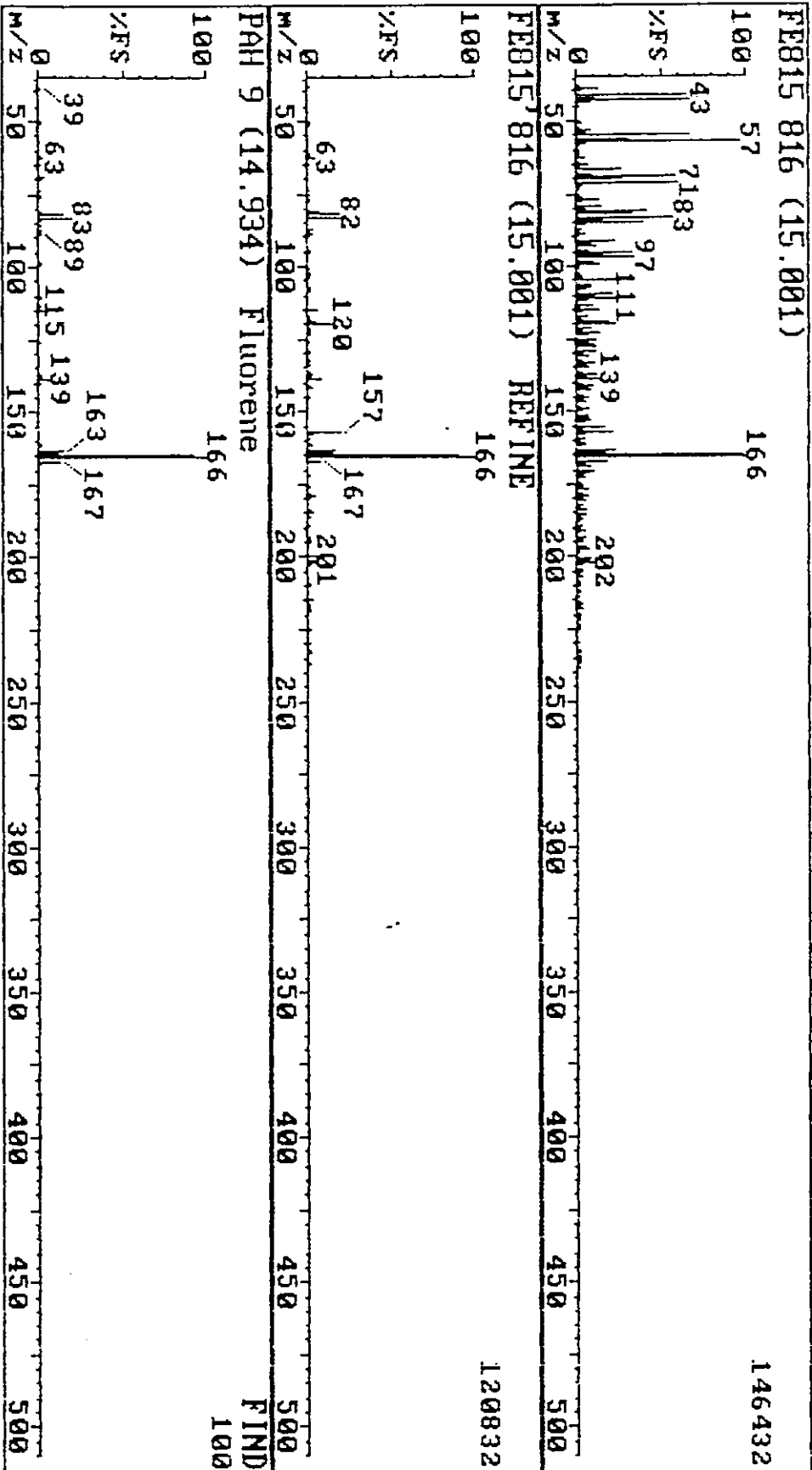


FIND
100

19-Sep-91 18:36
Sample: RUN#1 18976

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19-Sep-91 18:36

Triangle Labs, Inc.

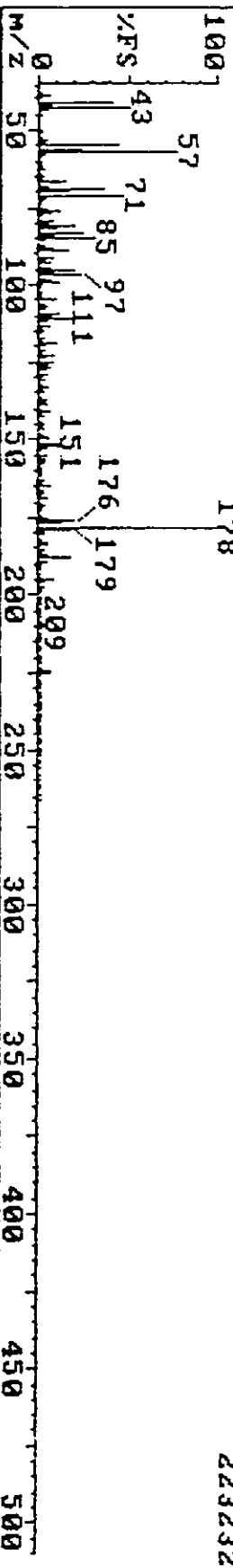
(919) 544-5729

Sample: RUN#1 18976

Instrument F

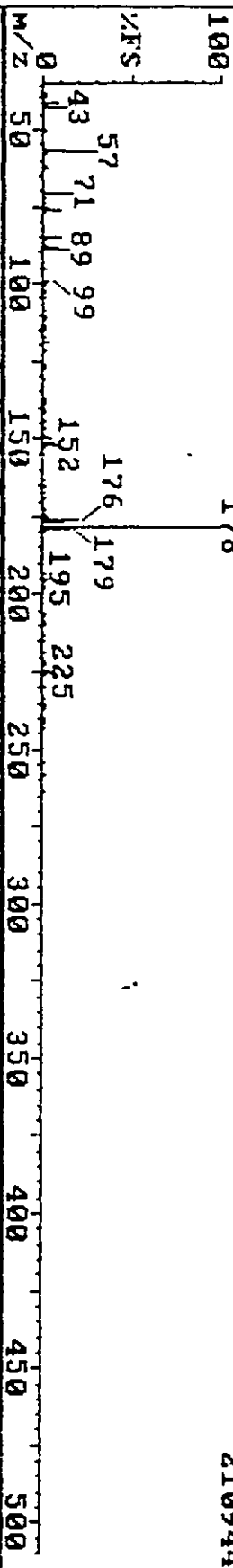
FE815 953 (17.284)

223232



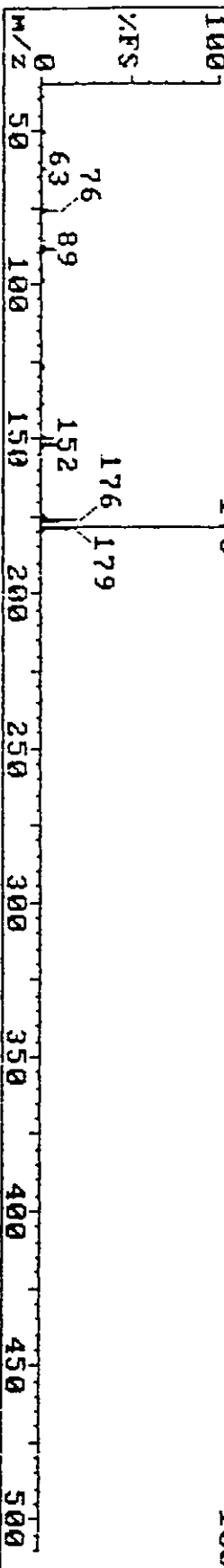
FE815 953 (17.284) REFINE

210944



PAH 11 (17.201) Phenanthrene

FIND 100



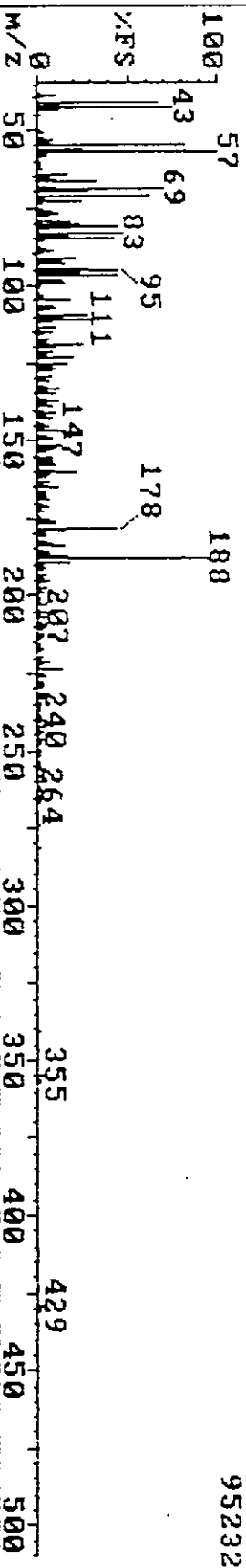
19-Sep-91 18:36

Sample: RUN#1 18976

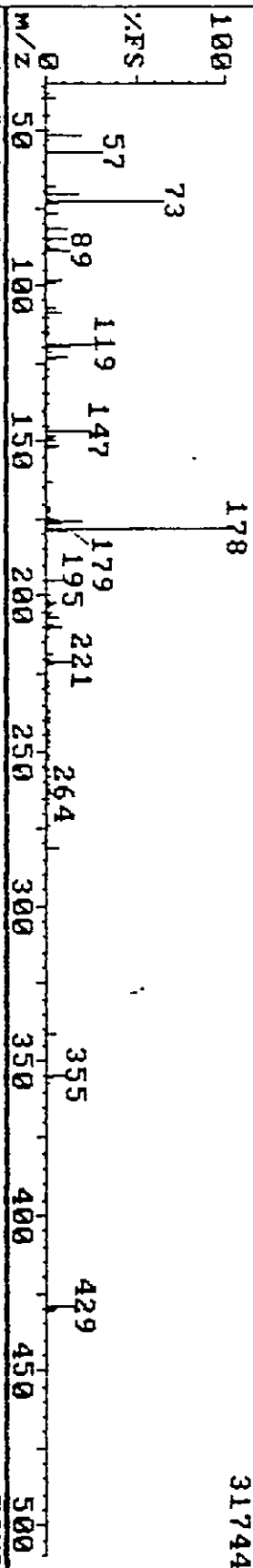
Triangle Labs, Inc.

(919) 544-5729
Instrument F

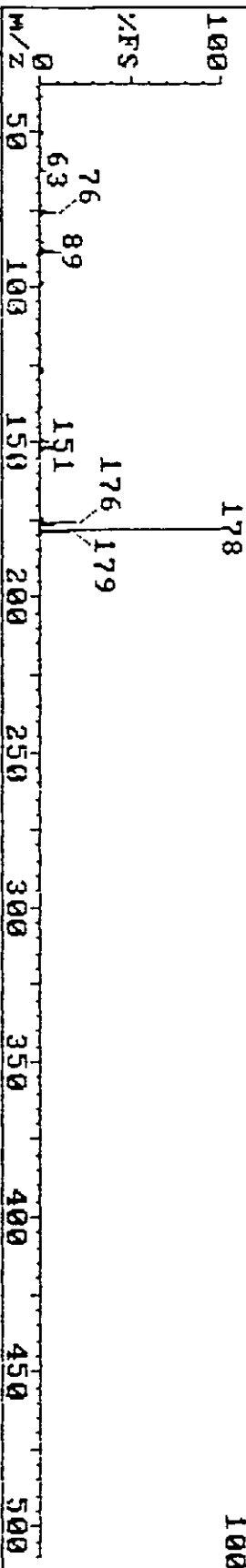
FEB15 960 (17.401)



FEB15 960 (17.401) REFINE



PAH 12 (17.334) Anthracene



FIND
100

31744

95232

19-Sep-91 18:36

Triangle Labs, Inc.

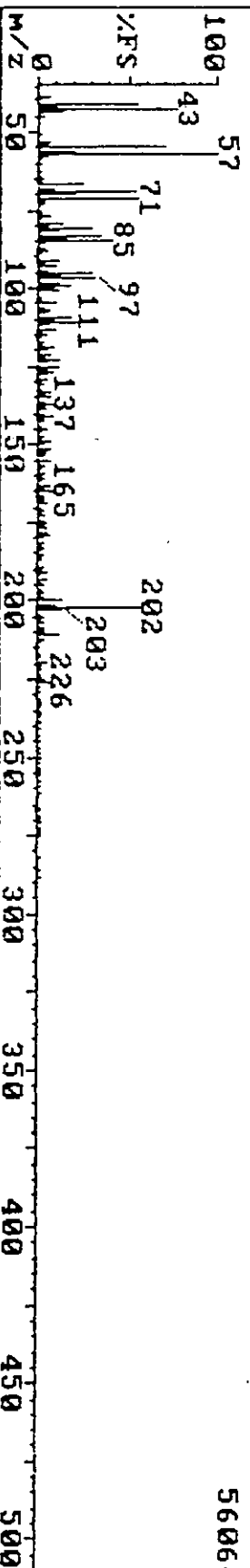
(919) 544-5729

Sample: RUN#1 18976

Instrument F

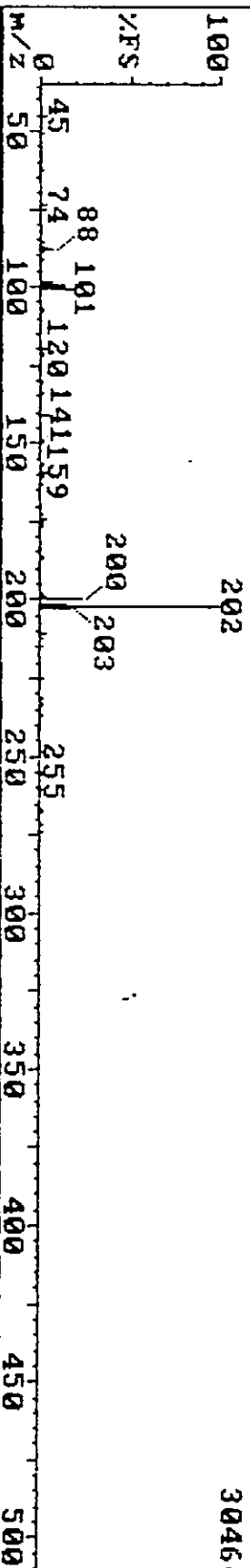
FEB15 1123 (20.118)

56064



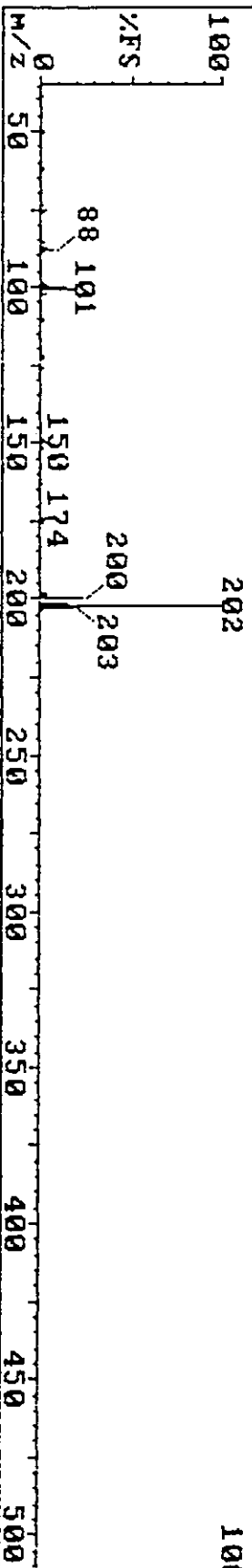
FEB15 1123 (20.117) REFINE

30464



PAH 13 (20.085) Fluoranthene

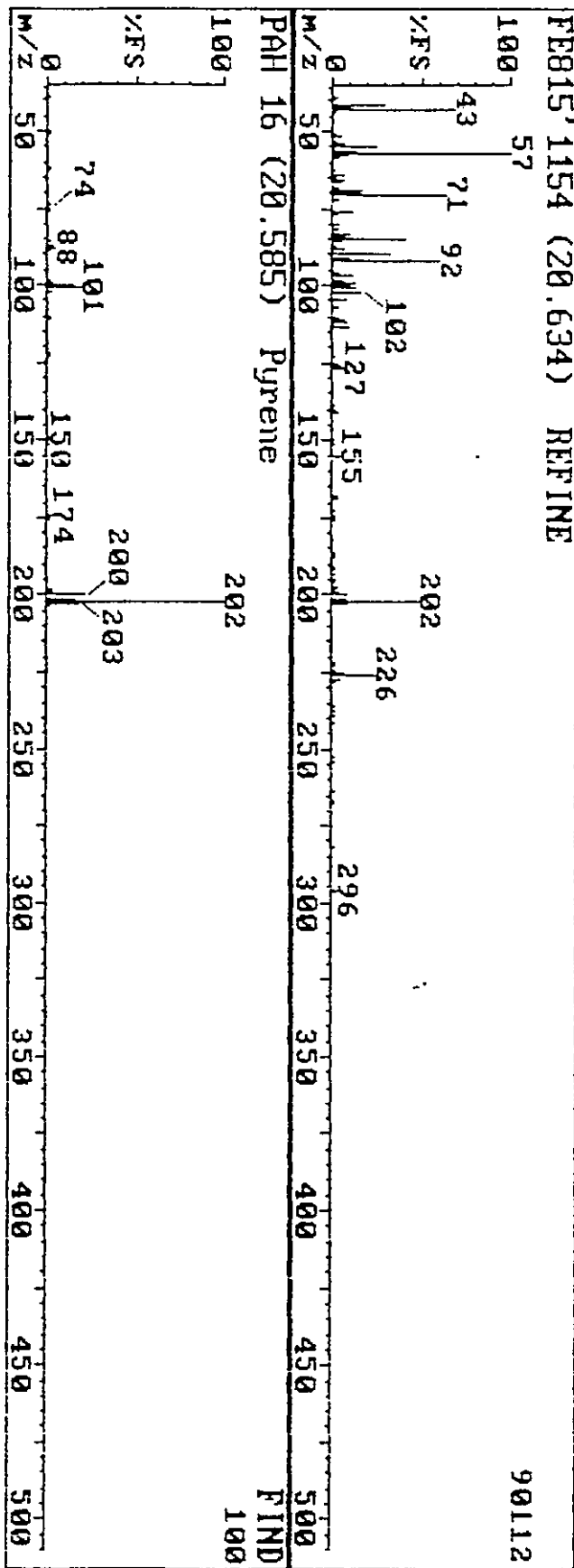
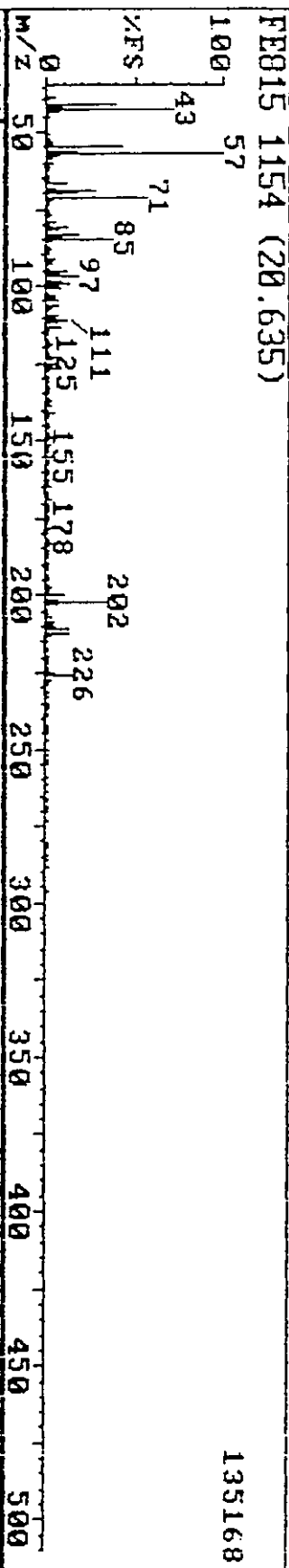
FIND
100



19-Sep-91 18:36
Sample: RUN#1 18976

Triangle Labs, Inc.

(919) 544-5729
Instrument F



TRIANGLE LABORATORIES, INC.
 801 Capitola Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE907
 RF FILE: FE901
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/25/91

SAMPLE ID: RUN #1 (1:4 dil.)
 DILN FACTOR: 4
 TLI Sample ID: 48.060.1A.H

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	1433		302	1		IS	
Naphthalene-d8	5092		478	14		IS	
Naphthalene	9158	.9408	480	14	305.86	D	40
2-Methylnaphthalene	3346	.7942	582	14	132.36	D	40
Acenaphthene-d10	3583		729	28		IS	
2-Chloronaphthalene	0	.9237	0	28	.97	ND	40
Acenaphthylene	3519	1.5395	707	28	102.05	D	40
Acenaphthene	0	.9778	0	28	.91	ND	40
Fluorene	921	1.1415	808	28	36.02	E	40
Phenanthrene-d10	7116		941	47		IS	
Phenanthrene	1195	.8666	943	47	31.01	E	40
Anthracene	0	.8724	0	47	.52	ND	40
Fluoranthene	193	1.3003	1113	47	3.33	E	40
Chrysene-d12	11953		1326	57		IS	
Pyrene	200	1.1620	1143	57	2.31	E	40
Benzo(a)anthracene	0	1.0992	0	57	.24	ND	40
Chrysene	0	1.0178	0	57	.26	ND	40
Perylene-d12	13687		1541	64		IS	
Benzo(b)fluoranthene	0	.9739	0	64	.24	ND	40
Benzo(k)fluoranthene	0	1.1928	0	64	.20	ND	40
Benzo(e)pyrene	0	.9749	0	64	.24	ND	40
Benzo(a)pyrene	0	1.0228	0	64	.23	ND	40
Perylene	0	.5802	0	64	.40	ND	40
Indeno(1,2,3-cd)pyrene	0	.8098	0	64	.29	ND	40
Dibenz(a,h)anthracene	0	.8430	0	64	.28	ND	40
Benzo(g,h,i)perylene	0	.9214	0	64	.25	ND	40

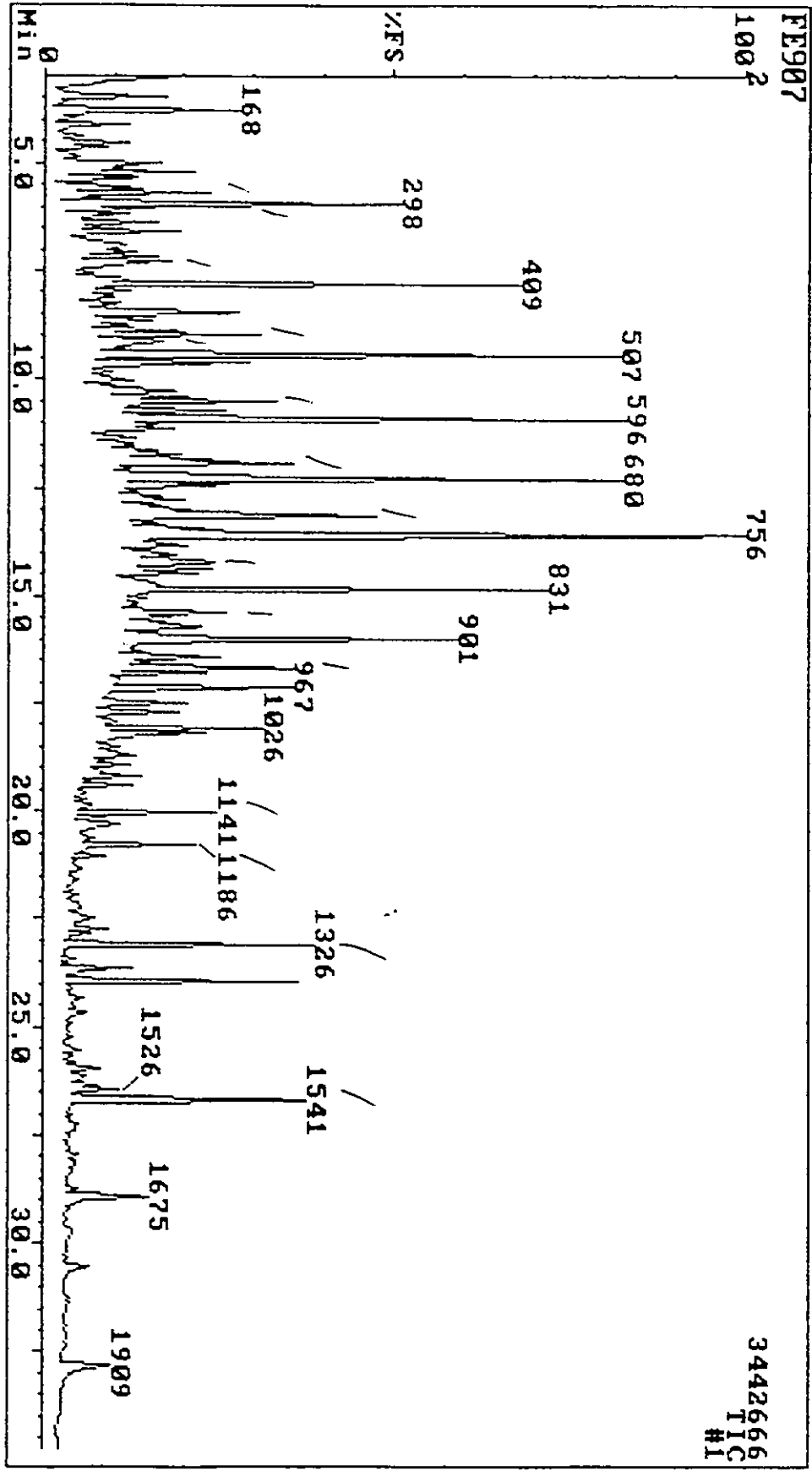
SURROGATE SUMMARY

	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14	4602	.8179	1186	57	75.31	D	75.3
Anthracene-d10	3327	.8804	948	47	84.95	D	85.0
Pyrene-d10	4763	.8714	1141	57	73.17	D	73.2
Phenol-d5	984	1.5876	273	1	69.18	D	69.2
2,4,6-Tribromophenol	248	.1108	843	28	100.00	D	100.0
1,4-Dibromobenzene-d4	478	.6186	488	1	86.24	D	86.2

25-Sep-91 13:34
Sample: RUN#1 (1:4 DIL.)

Triangle Labs, Inc.
18976

(919) 544-5729
Instrument F



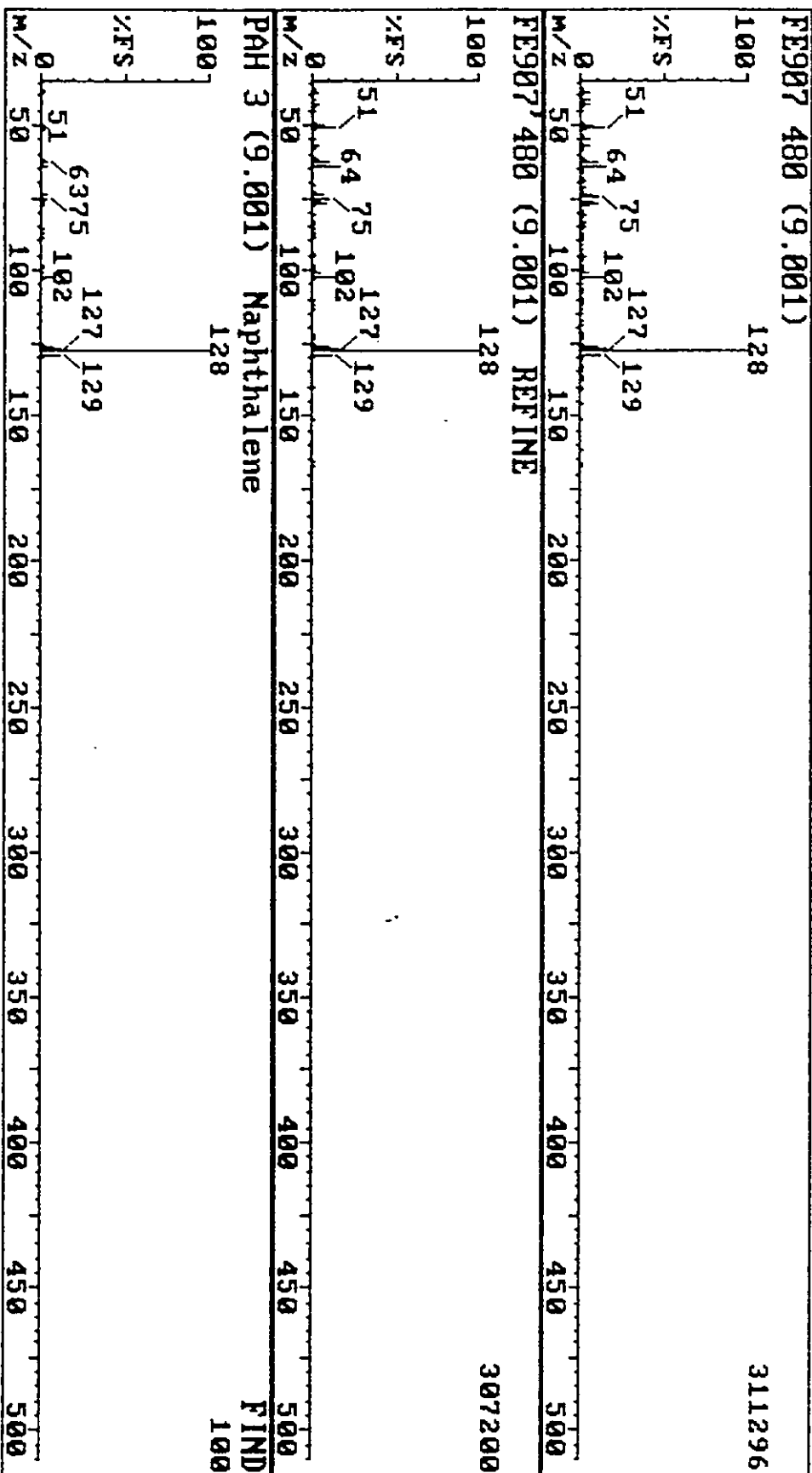
3442666
TIC
#1

MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	63	99	0	143280	bb	302 152 1,4 Dichlorobenzene-d4
2	76	44	87	1	509210	bb	478 136 Naphthalene-d8
3	97	73	94	-1	915800	bv	480 128 Naphthalene
4	93	59	89	0	334550	vb	582 142 2-Methylnaphthalene
5	86	47	91	0	358310	bv	729 164 Acenaphthene-d10
6	0	0	0	0	0	0	162 2-Chloronaphthalene
7	91	51	95	0	351850	vv	707 152 Acenaphthylene
8	0	0	0	0	0	0	153 Acenaphthene
9	63	30	79	-1	92083	vv	808 166 Fluorene
10	100	65	96	0	711650	vv	941 188 Phenanthrene-d10
11	64	27	93	-2	119540	vv	943 178 Phenanthrene
12	0	0	0	0	0	0	178 Anthracene
13	36	10	64	-3	19276	bb	1113 202 Fluoranthene
14	85	80	93	-3	1195300	bb	1326 240 Chrysene-d12
15	88	67	97	2	460160	bb	1186 244 Terphenyl-d14
16	53	12	72	0	20016	bb	1143 202 Pyrene
17	0	0	0	0	0	0	228 Benzo(a)anthracene
18	0	0	0	0	0	0	228 Chrysene
19	91	78	92	2	1368700	bv	1541 264 Perylene-d12
20	0	0	0	0	0	0	252 Benzo(b)fluoranthene
21	0	0	0	0	0	0	252 Benzo(k)fluoranthene
22	0	0	0	0	0	0	252 Benzo(e)pyrene
23	0	0	0	0	0	0	252 Benzo(a)pyrene
24	0	0	0	0	0	0	252 Perylene
25	0	0	0	0	0	0	276 Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0	0	278 Dibenz(a,h)anthracene
27	0	0	0	0	0	0	276 Benzo(g,h,i)perylene
28	0	0	0	0	0	0	266 Pentachlorophenol
29	76	44	86	-1	147460	vv	381 82 Nitrobenzene-d5
30	66	38	76	-1	156500	bb	643 172 2-Fluorobiphenyl
31	61	27	86	-2	24812	bb	843 330 2,4,6-Tribromophenol
32	83	44	89	0	98356	bb	273 99 Phenol-d5
33	96	69	96	1	476300	vv	1141 212 Pyrene-d10
34	78	50	96	-2	332670	vb	948 188 Anthracene-d10
35	73	27	89	0	47772	bb	486 240 1,4-Dibromobenzene-d4
36	68	35	74	0	54032	bb	428 185 1,3,5-Trichlorobenzene-d3

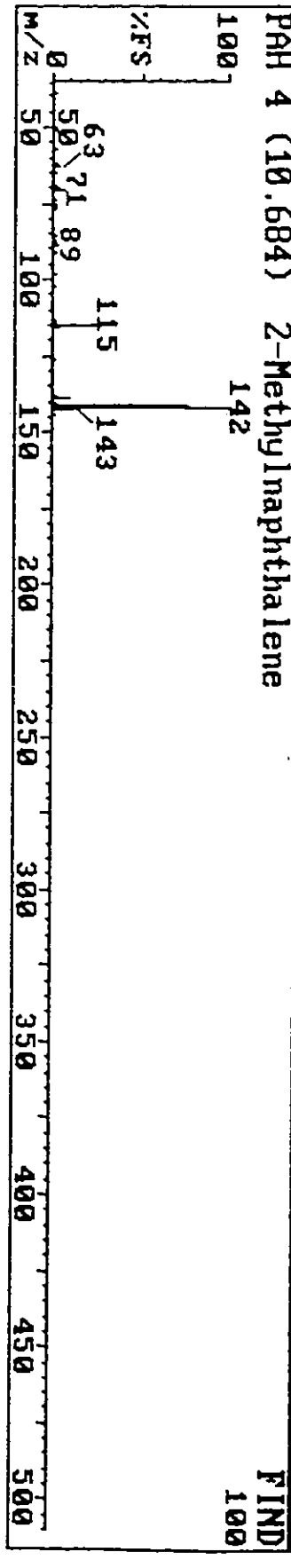
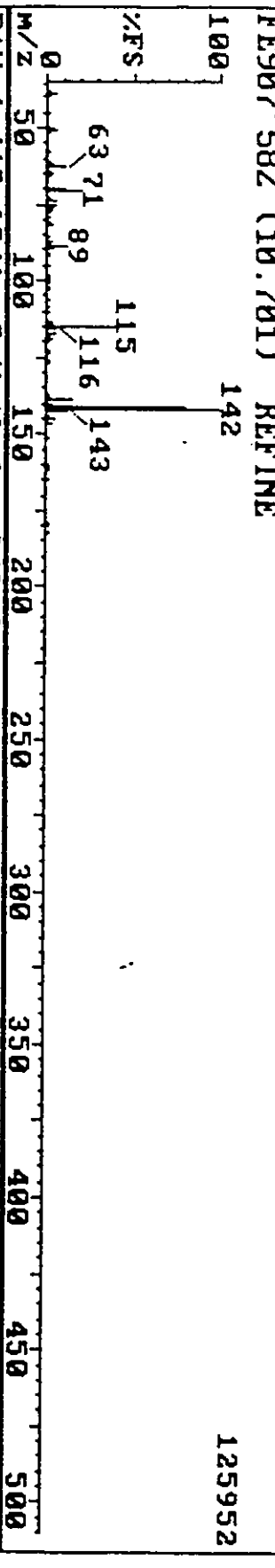
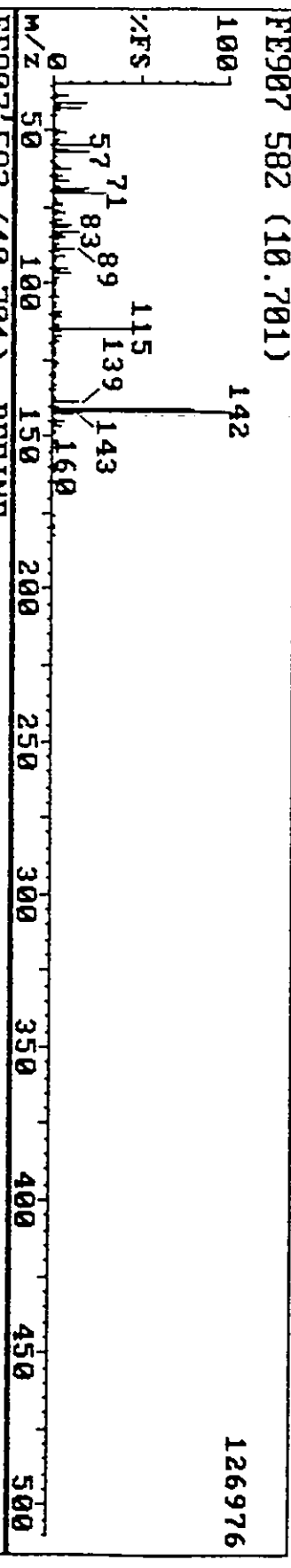
25-Sep-91 13:34
Sample: RUN#1 (1:4 DIL.)

Triangle Labs, Inc.
18976

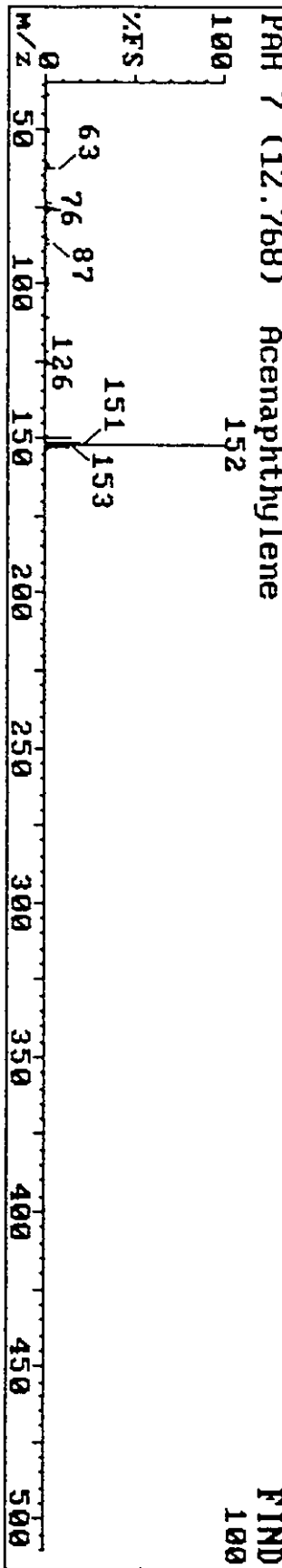
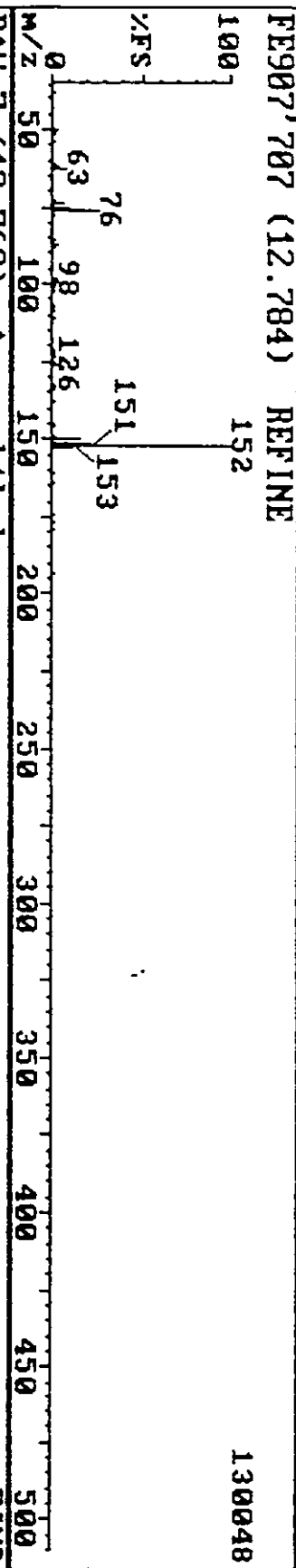
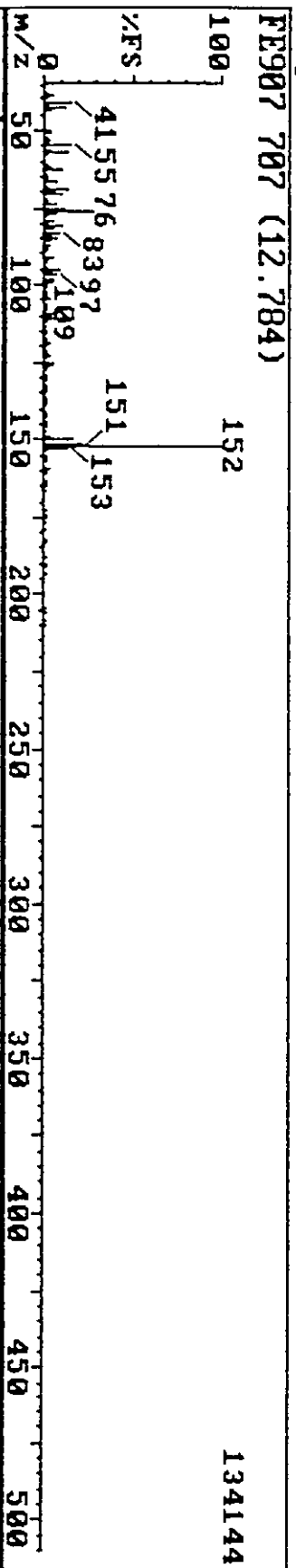
(919) 544-5729
Instrument F



25-Sep-91 13:34 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#1 (1:4 DIL.) 18976 Instrument F



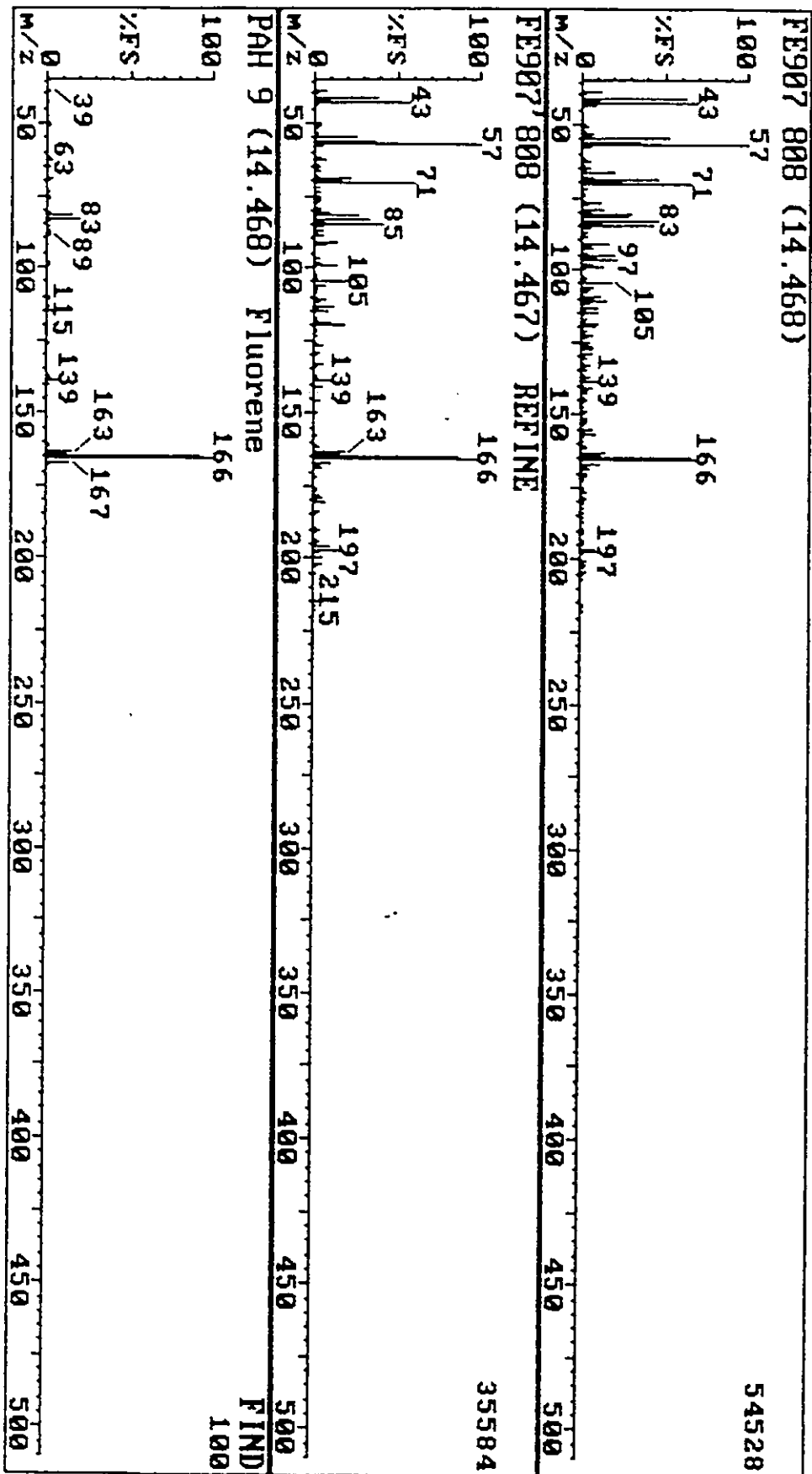
25-Sep-91 13:34 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#1 (1:4 DIL.) 18976 Instrument F



25-Sep-91 13:34
Sample: RUN#1 (1:4 DIL.)

Triangle Labs, Inc.
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(919) 544-5729
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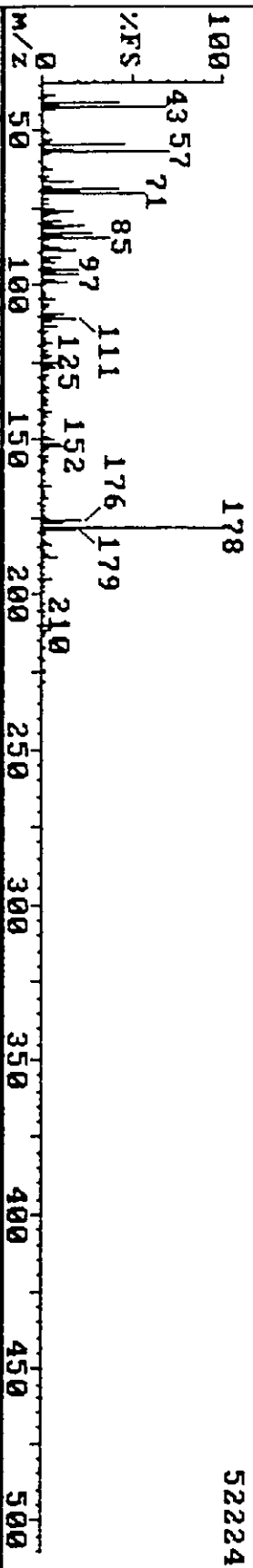


25-Sep-91 13:34
Sample: RUN#1 (1:4 DIL.)

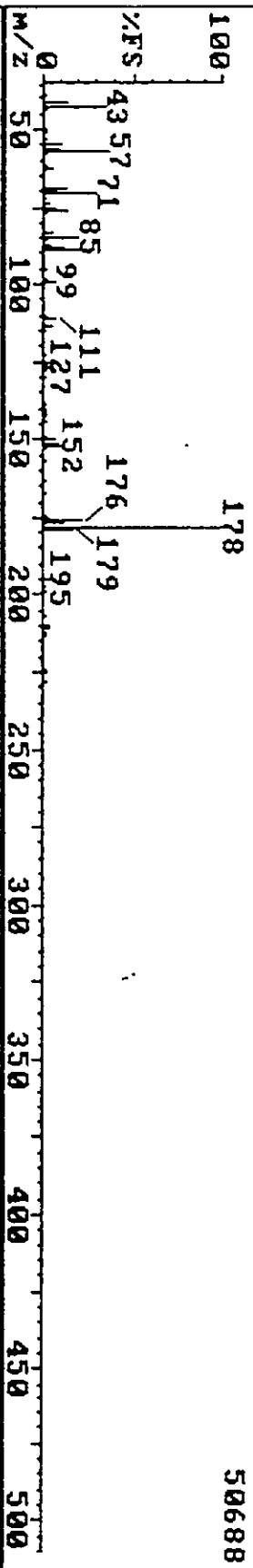
Triangle Labs, Inc.
18976

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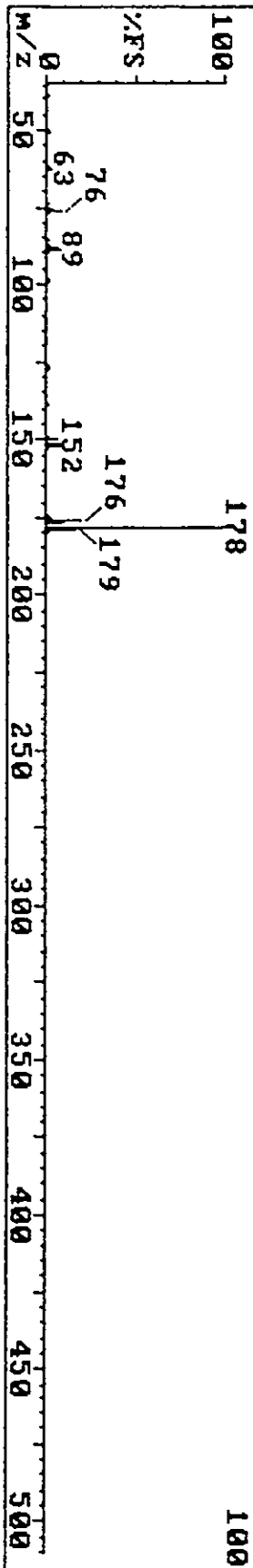
FE907 943 (16.718)



FE907 943 (16.717) REFINE



PAH 11 (16.734) Phenanthrene

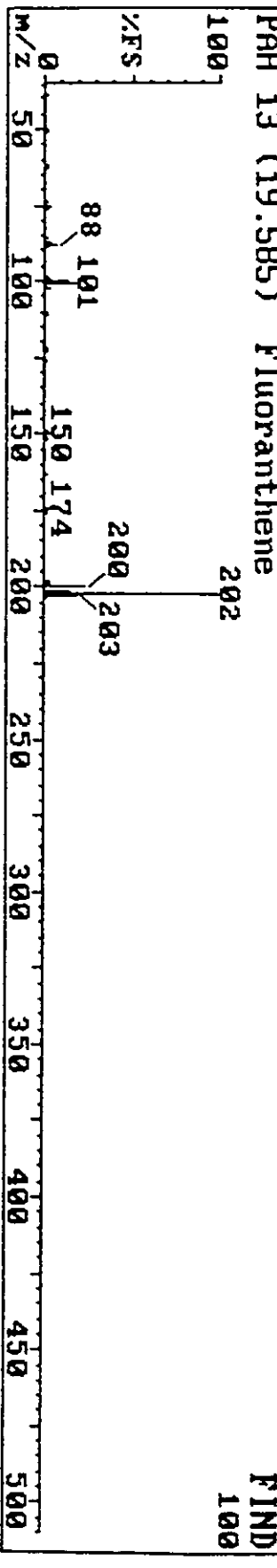
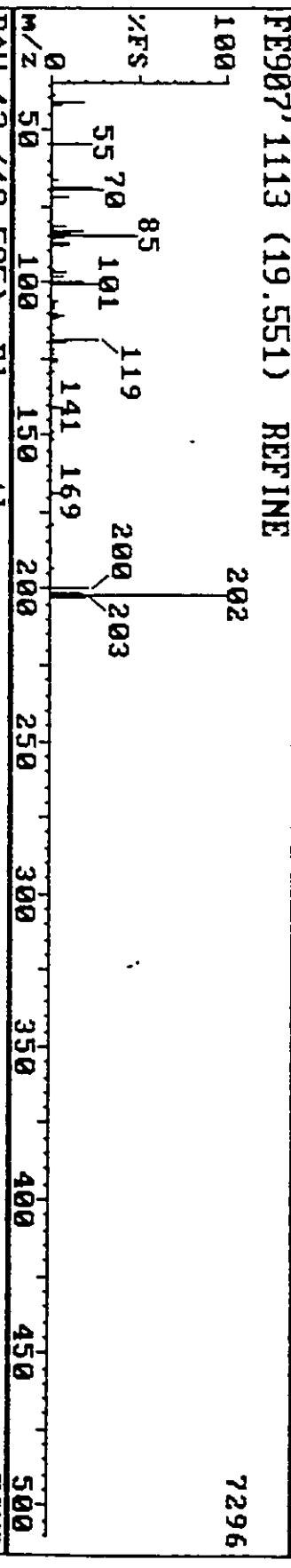
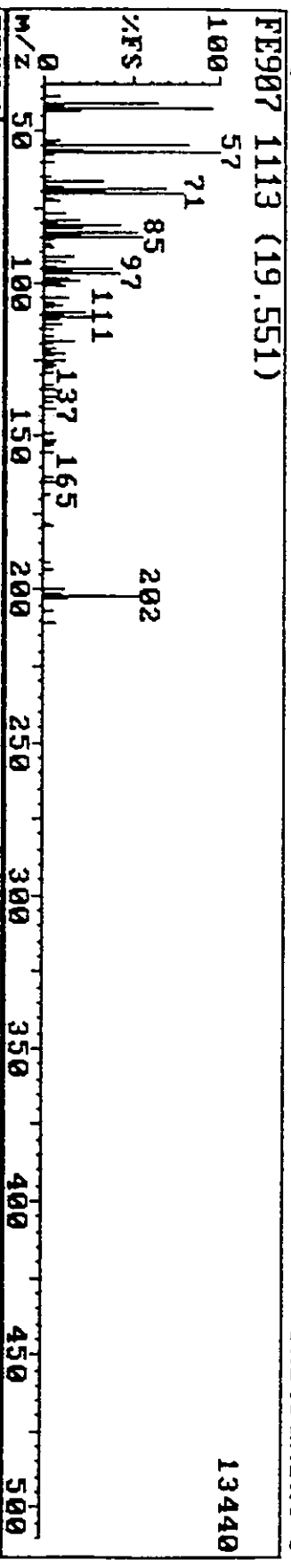


FIND
100

50688

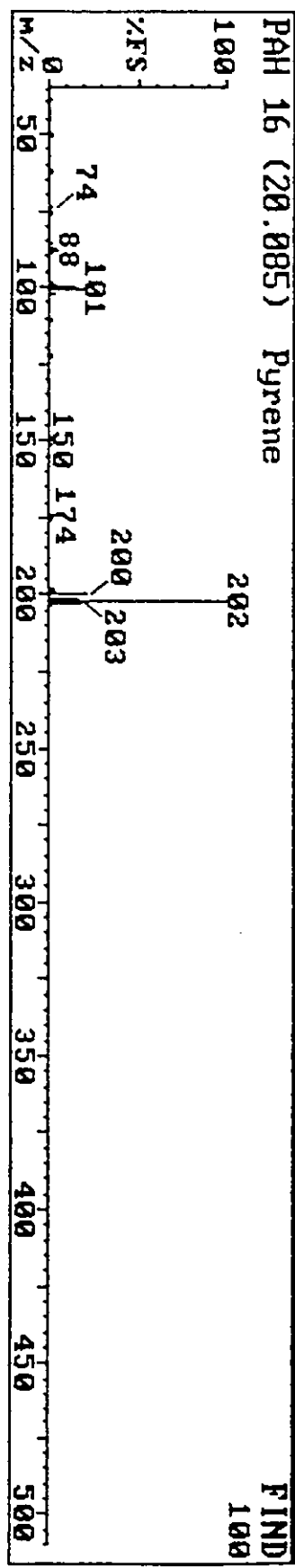
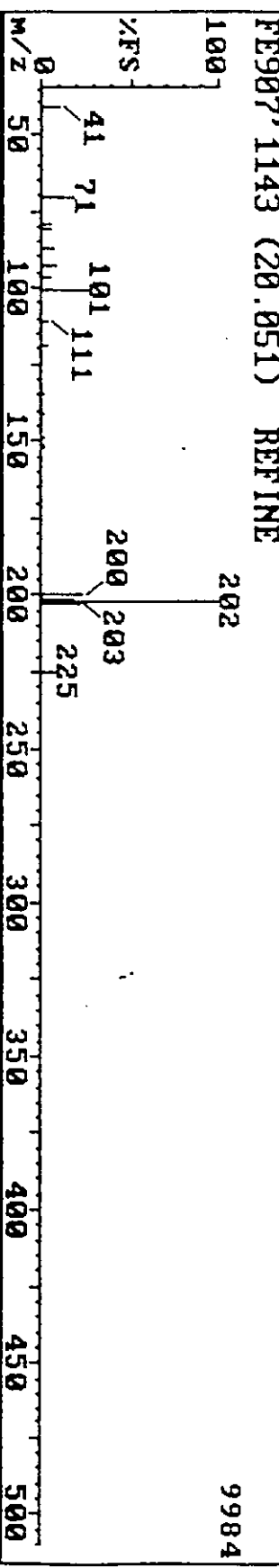
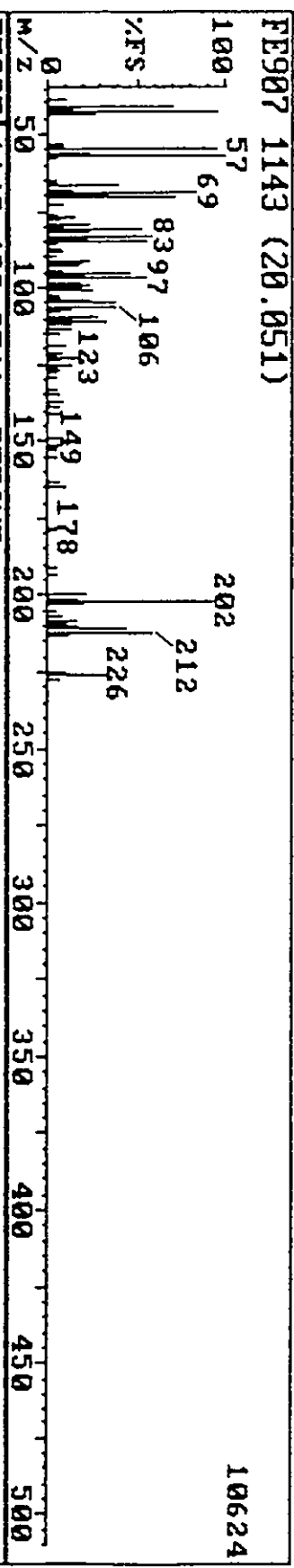
52224

25-Sep-91 13:34 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#1 (1:4 DIL.) 18976 Instrument F



25-Sep-91 13:34
Sample: RUN#1 (1:4 DIL.)
Triangle Labs, Inc.
18976
(919) 544-5729
Instrument F

314



FIND
100

9984

10624

TRIANGLE LABORATORIES, INC.
 801 Capitola Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE816
 RF FILE: FE807
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/19/91

SAMPLE ID: RUN #2
 DILN FACTOR: 1
 TLI Sample ID: 46.061.1A.H

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	2044		308	1		IS	
Naphthalene-d8	8050		483	14		IS	
Naphthalene	47772	.9104	487	14	260.75	D	10
2-Methylnaphthalene	17901	.7186	588	14	123.78	D	10
Acenaphthene-d10	5550		736	28		IS	
2-Chloronaphthalene	0	.9327	0	28	.15	ND	10
Acenaphthylene	18268	1.5120	714	28	87.07	D	10
Acenaphthene	0	1.0072	0	28	.14	ND	10
Fluorene	5627	.9405	816	28	43.12	D	10
Phenanthrene-d10	9611		950	47		IS	
Phenanthrene	7006	1.0774	953	47	27.06	D	10
Anthracene	0	1.0176	0	47	.08	ND	10
Fluoranthene	886	1.1700	1123	47	3.15	E	10
Chrysene-d12	8941		1338	57		IS	
Pyrene	0	.9377	0	57	.10	ND	10
Benzo(a)anthracene	0	1.0234	0	57	.09	ND	10
Chrysene	0	1.0396	0	57	.09	ND	10
Perylene-d12	8628		1557	64		IS	
Benzo(b)fluoranthene	0	.8831	0	64	.10	ND	10
Benzo(k)fluoranthene	0	.9783	0	64	.09	ND	10
Benzo(e)pyrene	0	.8487	0	64	.11	ND	10
Benzo(a)pyrene	0	.9448	0	64	.10	ND	10
Perylene	0	.5627	0	64	.16	ND	10
Indeno(1,2,3-cd)pyrene	0	.8595	0	64	.11	ND	10
Dibenz(a,h)anthracene	0	.9225	0	64	.10	ND	10
Benzo(g,h,i)perylene	0	.9620	0	64	.10	ND	10

SURROGATE SUMMARY

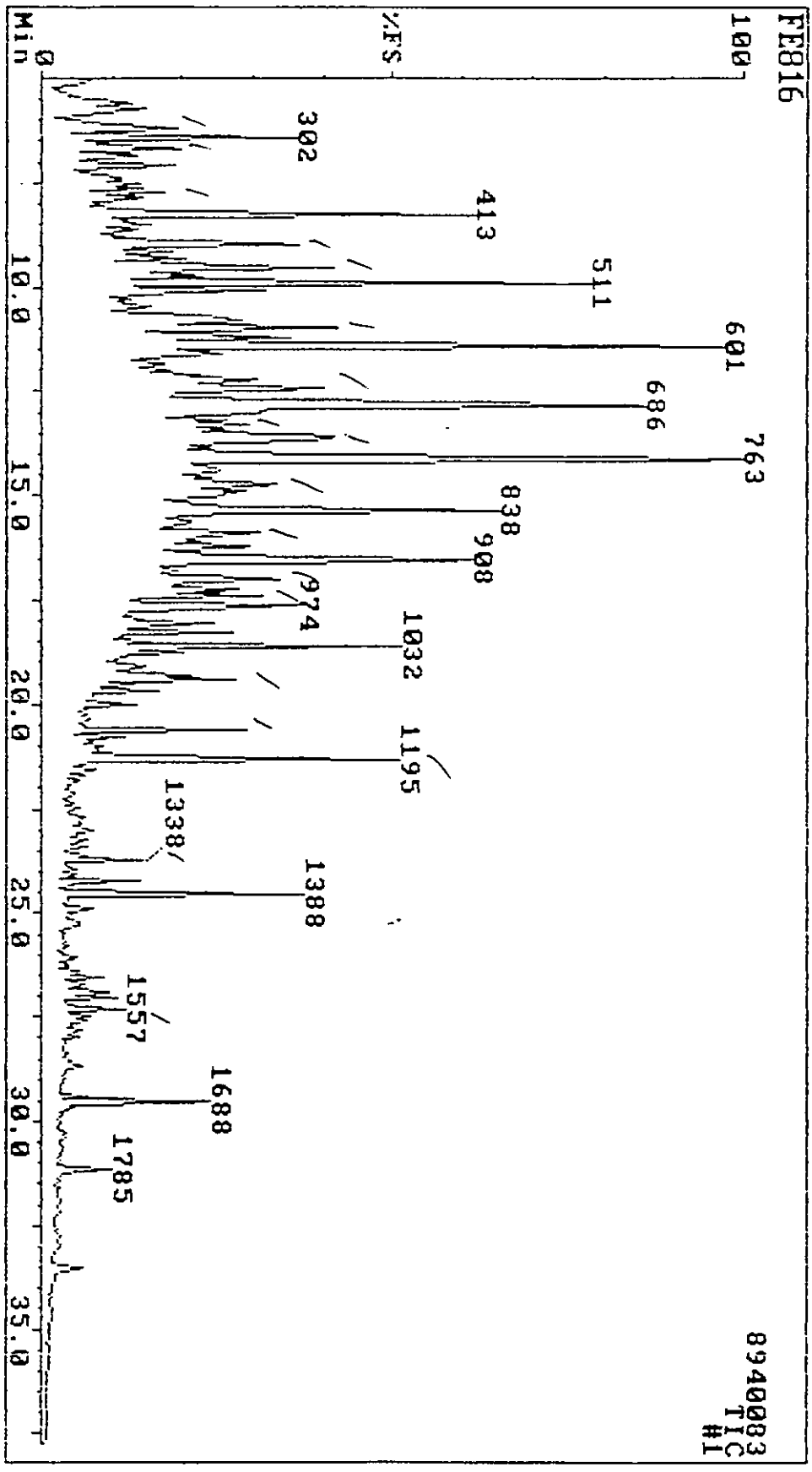
	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14	18824	.6288	1195	57	133.92	D	133.9
Anthracene-d10	17266	.9242	958	47	77.75	D	77.8
Pyrene-d10	20033	.6547	1152	57	136.89	D	136.9
Phenol-d5	4344	1.1959	282	1	71.10	D	71.1
2,4,6-Tribromophenol	2133	.0779	852	28	197.30	D	197.3
1,4-Dibromobenzene-d4	2593	.4696	491	1	108.04	D	108.0

CODES: ND = Not Detected; D = Detected; E = Estimated; IS = Internal Standard

19-Sep-91 19:24
Sample: RUN#2 18976

Triangle Labs, Inc.

(919) 544-5729
Instrument F



Date Review 9/30/91 *sc*

QUAN DB : FEB16

LAB-BASE QUAN

19-Sep-91

22:58

N	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	57	38	89	4	204360	bb	308	152 1,4-Dichlorobenzene-d4
2	54	28	81	-3	804960	vv	483	136 Naphthalene-d8
3	93	76	97	2	4777200	bv	487	128 Naphthalene
4	91	56	89	0	1790100	vv	588	142 2-Methylnaphthalene
5	68	27	81	0	555010	vv	736	164 Acenaphthene-d10
6	0	0	0	0	0		0	162 2-Chloronaphthalene
7	90	47	97	0	1826800	bv	714	152 Acenaphthylene
8	0	0	0	0	0		0	153 Acenaphthene
9	73	33	83	0	562670	vv	816	166 Fluorene
10	76	29	92	0	961120	vv	950	188 Phenanthrene-d10
11	78	29	95	0	700550	vv	953	178 Phenanthrene
12	49	10	75	-1	56702	vv	980	178 Anthracene
13	47	20	84	-4	88553	vv	1123	202 Fluoranthene
14	56	62	94	-6	894120	bb	1338	240 Chrysene-d12
15	74	42	96	2	1882400	vb	1195	244 Terphenyl-d14
16	58	19	89	2	81705	vv	1154	202 Pyrene
17	0	0	0	0	0		0	228 Benzo(a)anthracene
18	0	0	0	0	0		0	228 Chrysene
19	89	61	93	1	862810	bb	1557	264 Perylene-d12
20	0	0	0	0	0		0	252 Benzo(b)fluoranthene
21	0	0	0	0	0		0	252 Benzo(k)fluoranthene
22	0	0	0	0	0		0	252 Benzo(e)pyrene
23	0	0	0	0	0		0	252 Benzo(a)pyrene
24	0	0	0	0	0		0	252 Perylene
25	0	0	0	0	0		0	276 Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0		0	278 Dibenz(a,h)anthracene
27	0	0	0	0	0		0	276 Benzo(g,h,i)perylene
28	0	0	0	0	0		0	266 Pentachlorophenol
29	70	43	88	2	414800	vv	386	82 Nitrobenzene-d5
30	69	39	79	-1	970360	bv	648	172 2-Fluorobiphenyl
31	67	23	84	0	213260	bb	852	330 2,4,6-Tribromophenol
32	58	41	88	5	434430	vb	282	99 Phenol-d5
33	81	67	97	3	2003300	vv	1152	212 Pyrene-d10
34	93	52	97	0	1726600	vv	958	188 Anthracene-d10
35	57	23	93	-3	259310	bb	491	240 1,4-Dibromobenzene-d4
36	66	35	79	1	301250	bb	433	185 1,3,5-Trichlorobenzene-d3

19-Sep-91 19:24

Sample: RUN#2 18976

Triangle Labs, Inc.

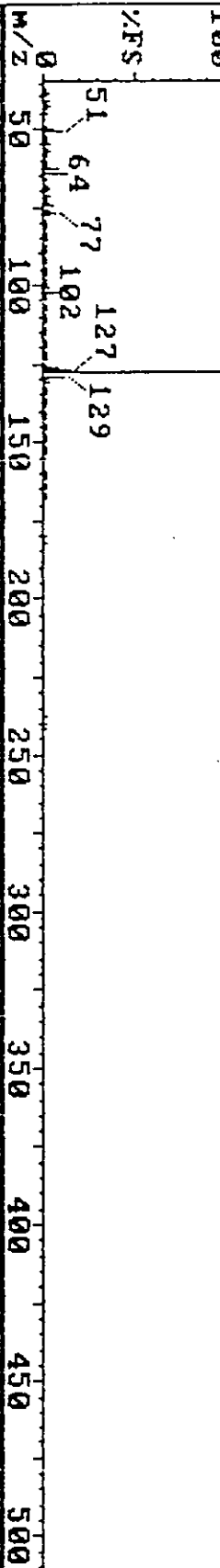
(919) 544-5729

Instrument F

FEB16 487 (9.517)

128

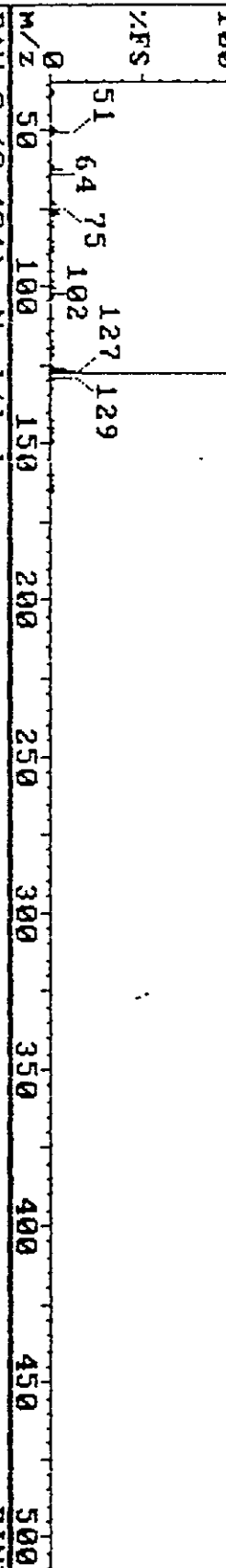
1261568



FEB16 487 (9.517) REFINE

128

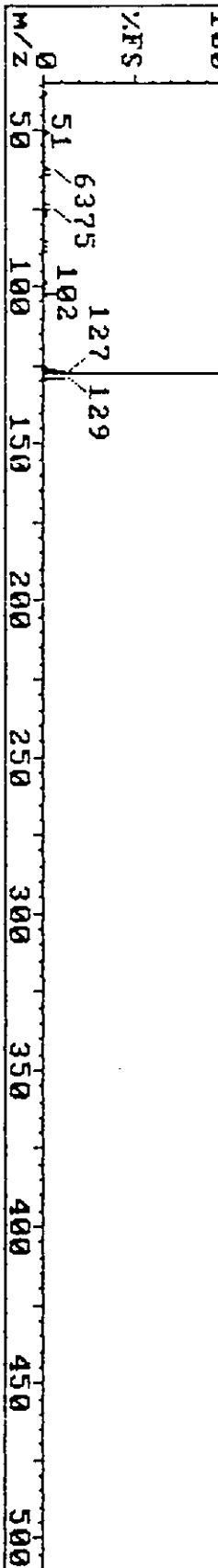
1228800



PAH 3 (9.434) Naphthalene

128

FIND 100



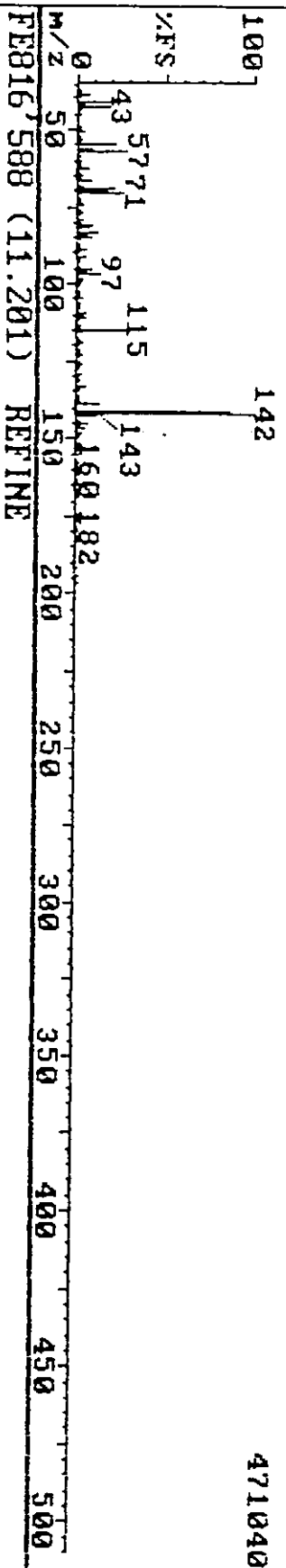
19-Sep-91 19:24

Sample: RUN#2 18976

Triangle Labs, Inc.

(919) 544-5729
Instrument F

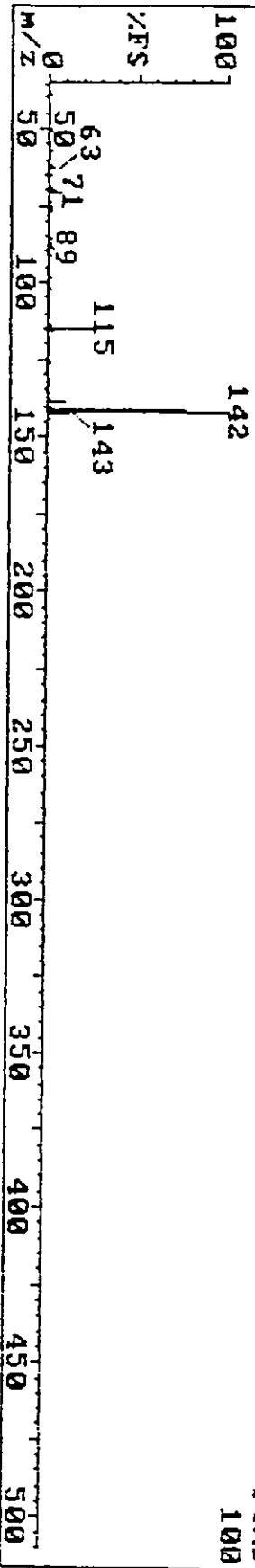
FEB16 588 (11.201)



FEB16 588 (11.201) REFINE

458752

PAH 4 (11.134) 2-Methylnaphthalene



FIND

100

19-Sep-91 19:24

Sample: RUN#2 18976

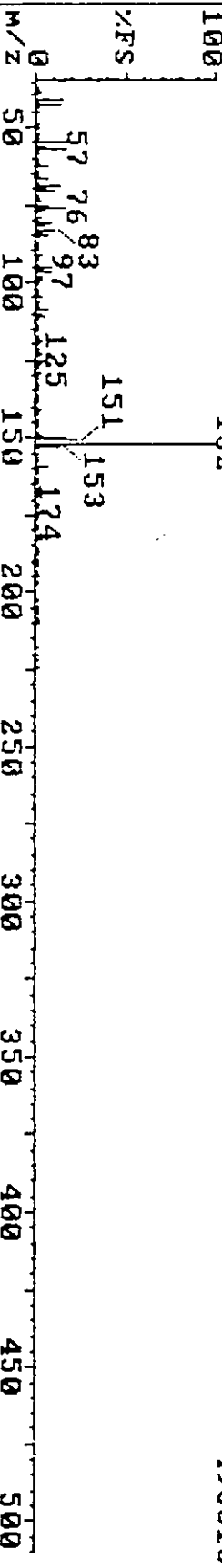
Triangle Labs, Inc.

(919) 544-5729
Instrument F

FE816 714 (13.301)

152

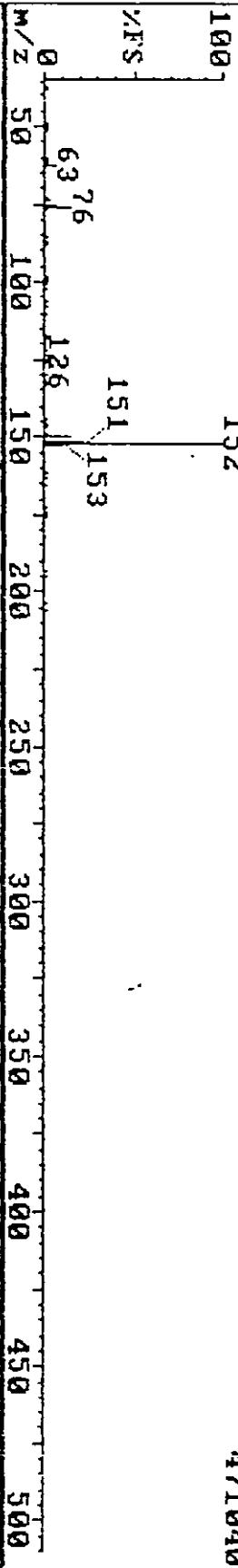
495616



FE816 714 (13.301) REFINE

152

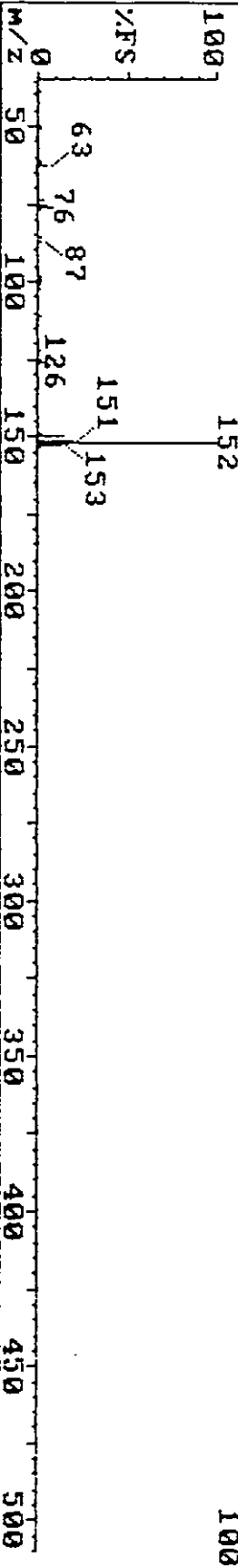
471040



PAH 7 (13.234) Acenaphthylene

152

FIND

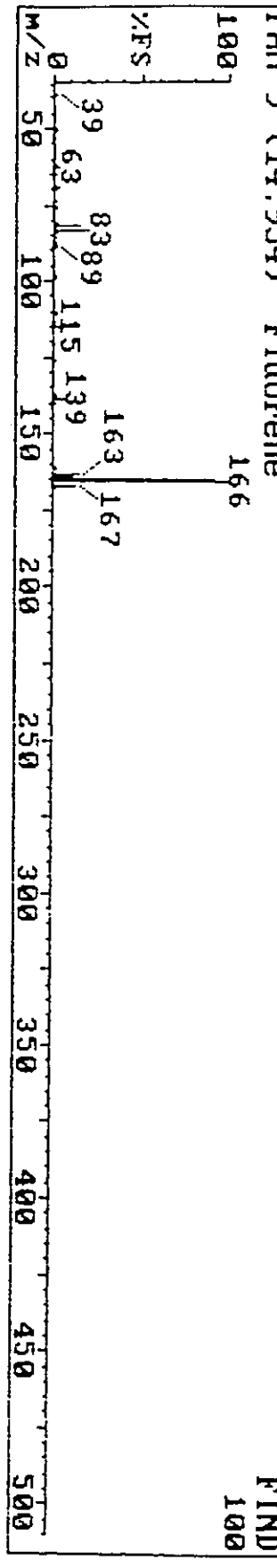
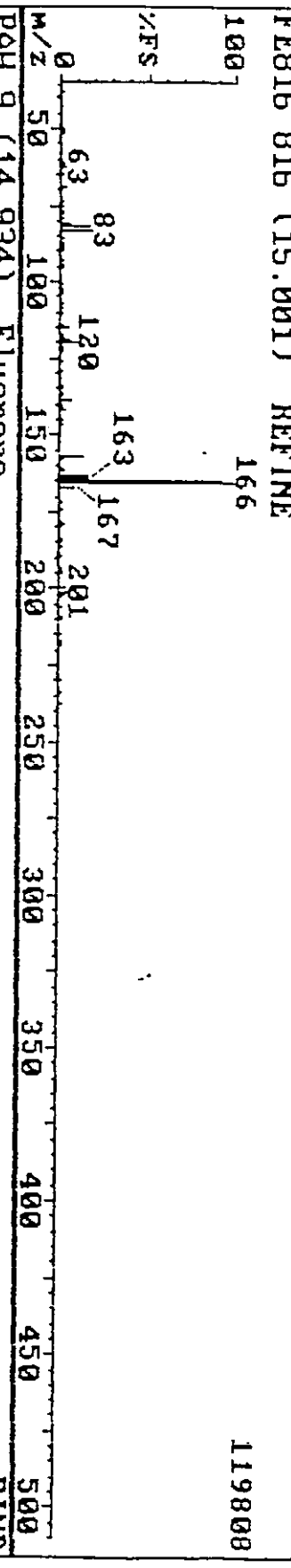
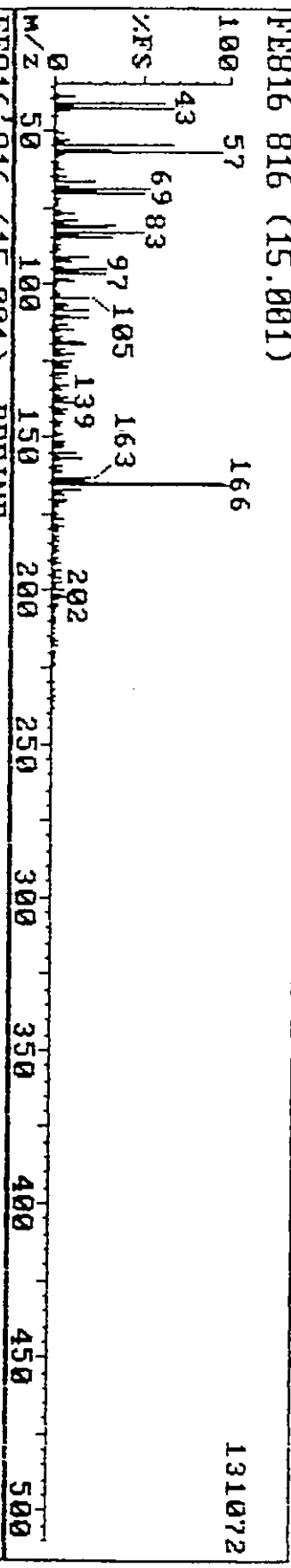


19-Sep-91 19:24

Sample: RUN#2 18976

Triangle Labs, Inc.

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Instrument F



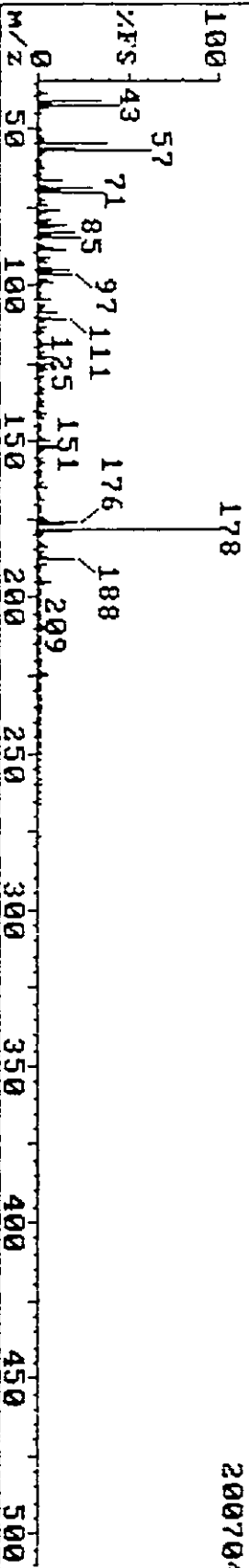
19-Sep-91 19:24

Sample: RUN#2 18976

Triangle Labs, Inc.

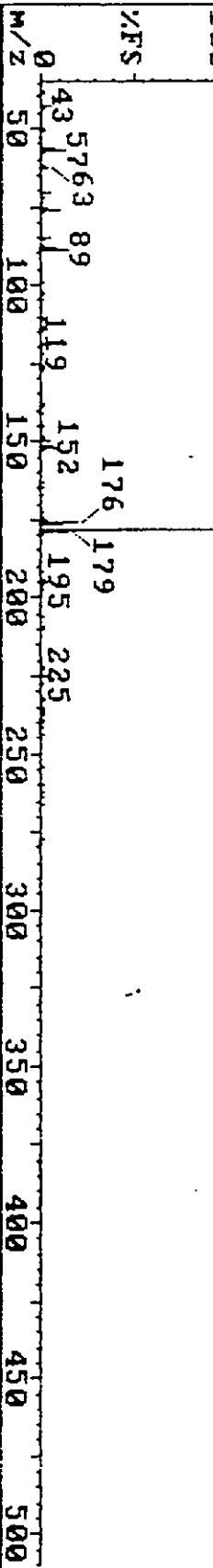
(919) 544-5729
Instrument F

FEB16 953 (17.284)



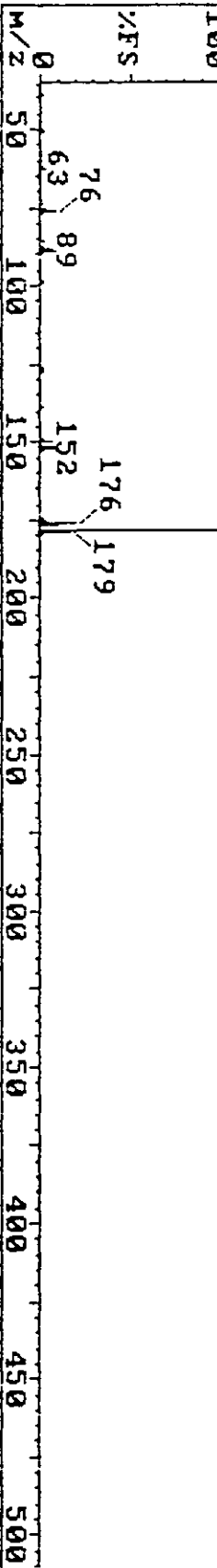
FEB16 953 (17.284) REFINE

191488



PAH 11 (17.281) Phenanthrene

FIND 100



19-Sep-91 19:24

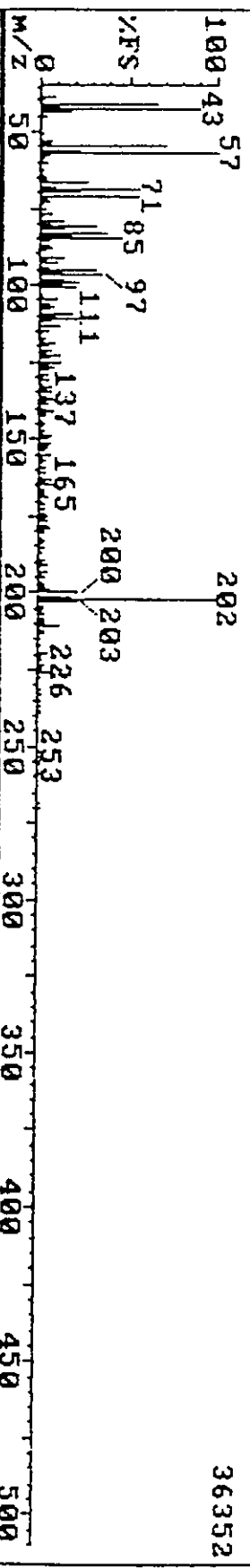
Triangle Labs, Inc.

(919) 544-5729

Sample: RUNHZ 18976

Instrument F

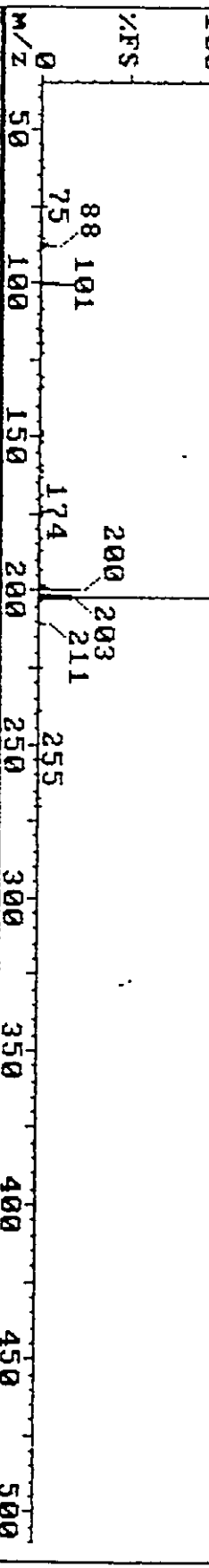
FEB16 1123 (20.118)



FEB16 1123 (20.117) REFINE

202

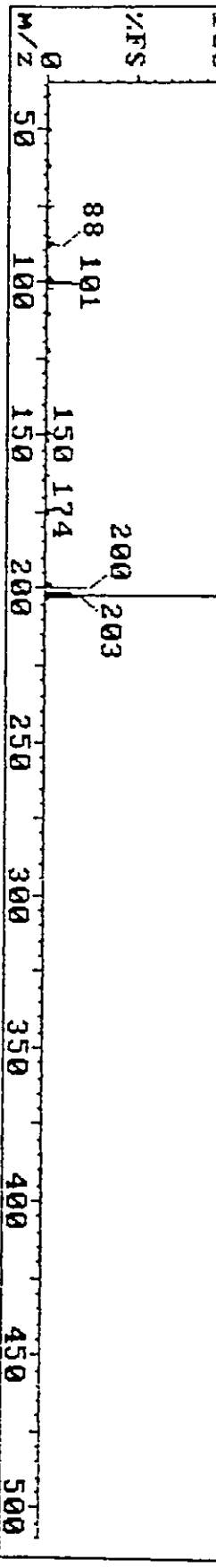
34816



PAH 13 (20.085) Fluoranthene

202

FIND 100



TRIANGLE LABORATORIES, INC.

801 Capitola Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE908
 RF FILE: FE901
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/25/91

SAMPLE ID: RUN #2 (1:2 dil.)
 DILN FACTOR: 2
 TLI Sample ID: 46.061.1A.H

QUANTITATION REPORT

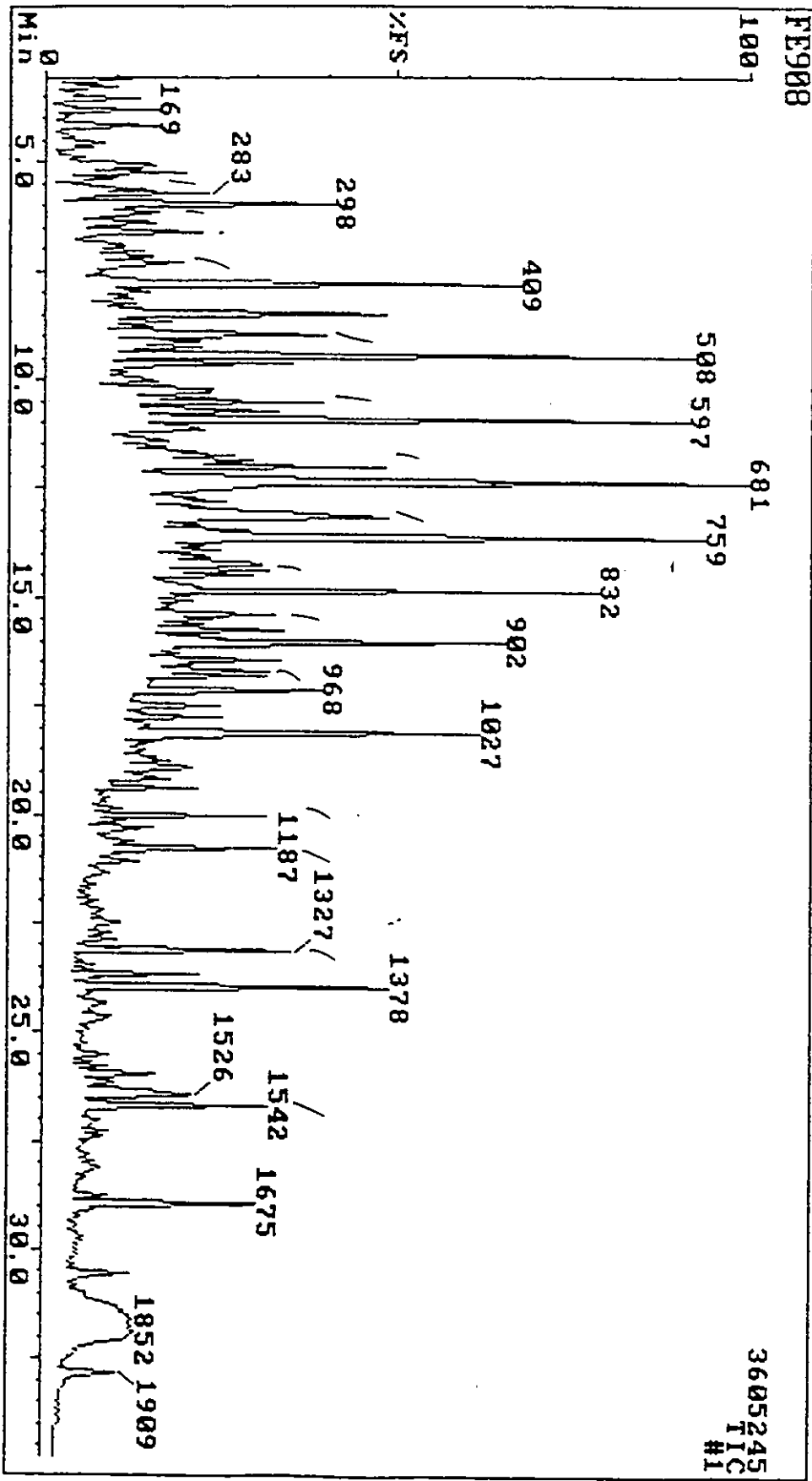
NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	1122		303	1		IS	
Naphthalene-d8	3940		478	14		IS	
Naphthalene	12301	.9408	481	14	265.44	D	20
2-Methylnaphthalene	4202	.7942	583	14	107.42	D	20
Acenaphthene-d10	2530		729	28		IS	
2-Chloronaphthalene	0	.9237	0	28	.68	ND	20
Acenaphthylene	4618	1.5395	708	28	94.85	D	20
Acenaphthene	0	.9778	0	28	.65	ND	20
Fluorene	1294	1.1415	809	28	35.84	D	20
Phenanthrene-d10	5541		941	47		IS	
Phenanthrene	1929	.8666	944	47	32.13	D	20
Anthracene	0	.8724	0	47	.33	ND	20
Fluoranthene	407	1.3003	1114	47	4.52	E	20
Chrysene-d12	9719		1327	57		IS	
Pyrene	0	1.1620	0	57	.14	ND	20
Benzo(a)anthracene	0	1.0892	0	57	.15	ND	20
Chrysene	0	1.0178	0	57	.16	ND	20
Perylene-d12	11213		1542	64		IS	
Benzo(b)fluoranthene	0	.9739	0	64	.15	ND	20
Benzo(k)fluoranthene	0	1.1928	0	64	.12	ND	20
Benzo(e)pyrene	0	.9749	0	64	.15	ND	20
Benzo(a)pyrene	0	1.0228	0	64	.14	ND	20
Perylene	0	.5802	0	64	.25	ND	20
Indeno(1,2,3-cd)pyrene	0	.8098	0	64	.18	ND	20
Dibenz(a,h)anthracene	0	.8430	0	64	.17	ND	20
Benzo(g,h,i)perylene	0	.9214	0	64	.15	ND	20

SURROGATE	SUMMARY	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14		7711	.8179	1186	57	77.60	D	77.6
Anthracene-d10		4937	.8804	949	47	80.97	D	81.0
Pyrene-d10		7396	.8714	1142	57	69.86	D	69.9
Phenol-d5		1689	1.5876	276	1	75.89	D	75.9
2,4,6-Tribromophenol		576	.1108	844	28	164.48	D	164.5
1,4-Dibromobenzene-d4		770	.8186	486	1	88.82	D	88.8

25-Sep-91 14:11
Sample: RUN#2 (1:2 DIL.)

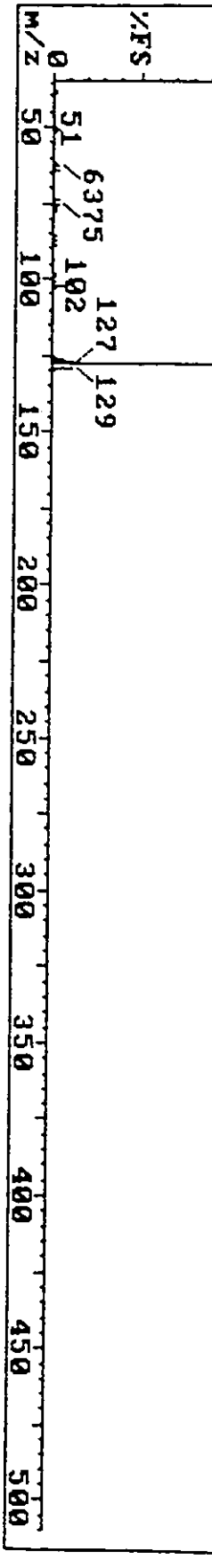
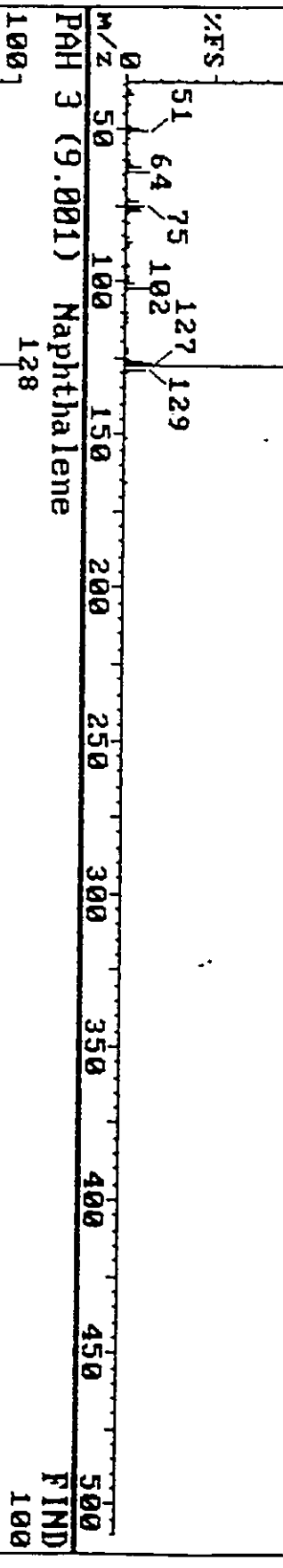
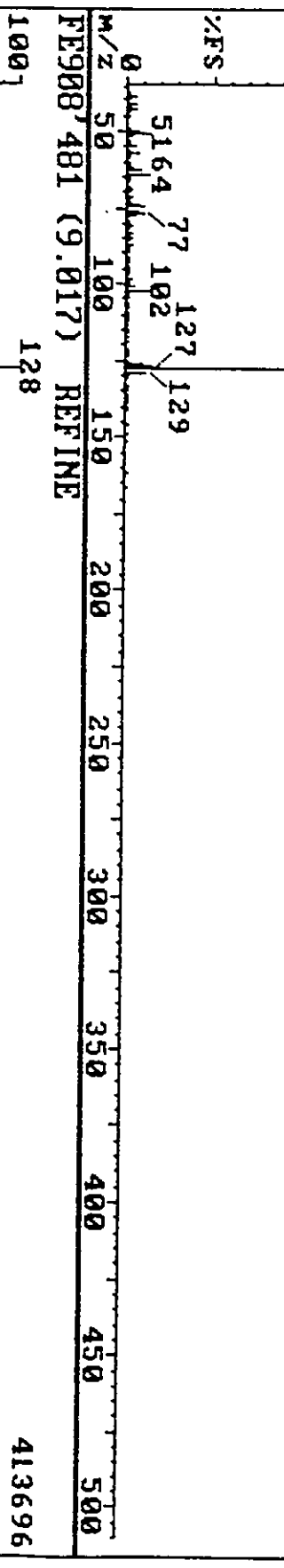
Triangle Labs, Inc.
18976

(919) 544-5729
Instrument F



I	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	92	60	98	1	112180	bb	303	152 1,4 Dichlorobenzene-d4
2	71	32	82	0	394040	bb	478	136 Naphthalene-d8
3	100	72	94	0	1230100	vv	481	128 Naphthalene
4	84	57	87	1	420200	vb	583	142 2-Methylnaphthalene
5	73	32	84	0	253010	vv	729	164 Acenaphthene-d10
6	0	0	0	0	0	0	0	162 2-Chloronaphthalene
7	81	46	93	1	461800	vv	708	152 Acenaphthylene
8	0	0	0	0	0	0	0	153 Acenaphthene
9	69	31	79	0	129400	vv	809	166 Fluorene
10	91	51	95	0	554080	vv	941	188 Phenanthrene-d10
11	73	32	94	-1	192870	vv	944	178 Phenanthrene
12	34	32	94	-8	192870	vv	944	178 Anthracene
13	52	17	80	-2	40672	vb	1114	202 Fluoranthene
14	89	73	93	-2	971860	bb	1327	240 Chrysene-d12
15	94	63	98	1	771050	bb	1186	244 Terphenyl-d14
16	66	21	85	0	Sc 75000	bb	1144	202 Pyrene
17	0	0	0	0	9/30/91 0	0	0	228 Benzo(a)anthracene
18	0	0	0	0	0	0	0	228 Chrysene
19	86	69	92	2	1121500	bb	1542	264 Perylene-d12
20	0	0	0	0	0	0	0	252 Benzo(b)fluoranthene
21	0	0	0	0	0	0	0	252 Benzo(k)fluoranthene
22	0	0	0	0	0	0	0	252 Benzo(e)pyrene
23	0	0	0	0	0	0	0	252 Benzo(a)pyrene
24	0	0	0	0	0	0	0	252 Perylene
25	0	0	0	0	0	0	0	276 Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0	0	0	278 Dibenz(a,h)anthracene
27	0	0	0	0	0	0	0	276 Benzo(g,h,i)perylene
28	0	0	0	0	0	0	0	266 Pentachlorophenol
29	83	53	90	-1	224800	vv	381	82 Nitrobenzene-d5
30	69	40	78	-1	233240	bb	643	172 2-Fluorobiphenyl
31	70	31	89	-1	57636	bb	844	330 2,4,6-Tribromophenol
32	83	51	92	2	168940	bb	276	99 Phenol-d5
33	97	69	98	1	739580	vv	1142	212 Pyrene-d10
34	85	50	96	-1	493700	vb	949	188 Anthracene-d10
35	67	27	89	-1	77044	bb	486	240 1,4-Dibromobenzene-d4
36	71	37	76	0	76976	bb	428	185 1,3,5-Trichlorobenzene-d3

25-Sep-91 14:11
Sample: RUN#2 (1:2 DIL.)
Triangle Labs, Inc.
18976
(919) 544-5729
Instrument F



25-Sep-91 14:11

Triangle Labs, Inc.

(919) 544-5729

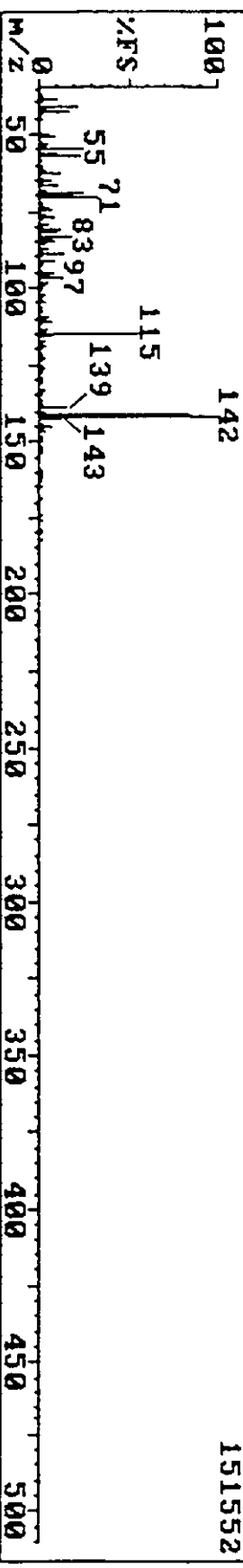
Sample: RUN#2 (1:2 DIL.)

18976

Instrument F

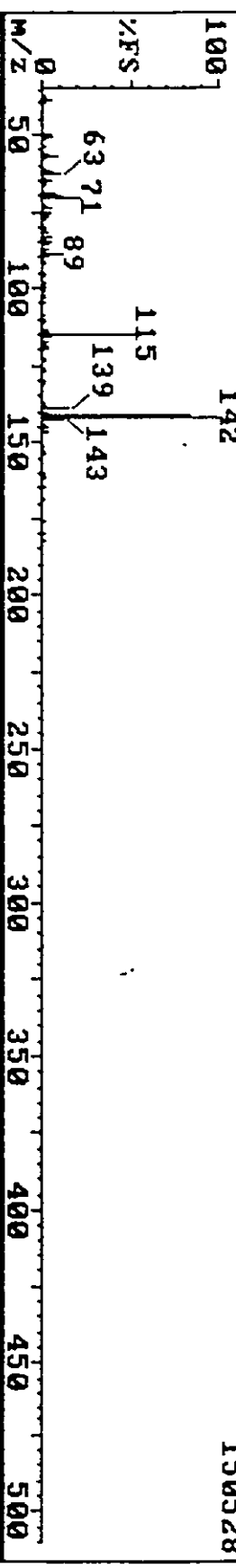
FE908 583 (10.717)

151552



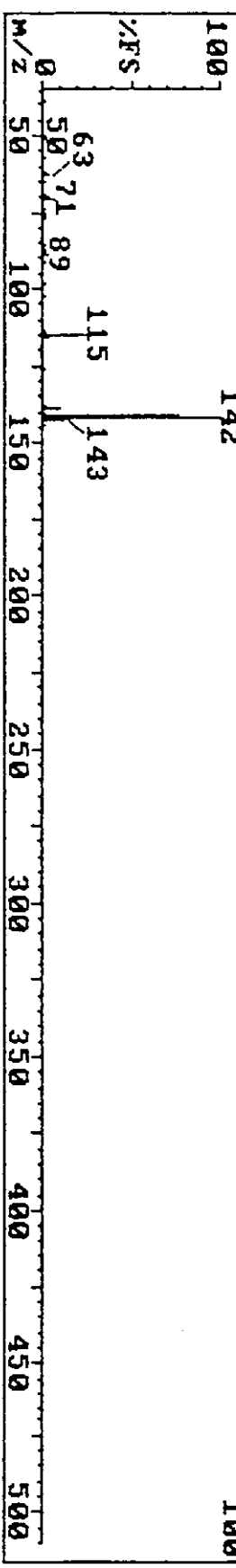
FE908 583 (10.717) REFINE

150528

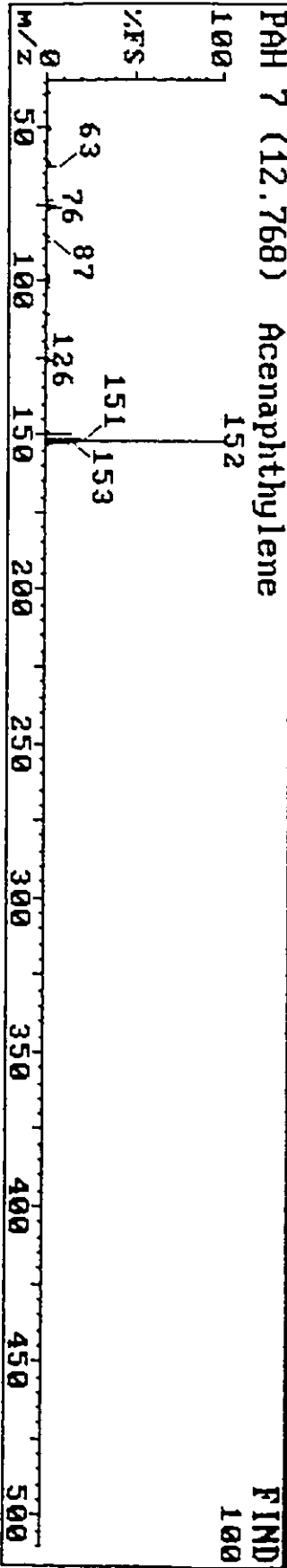
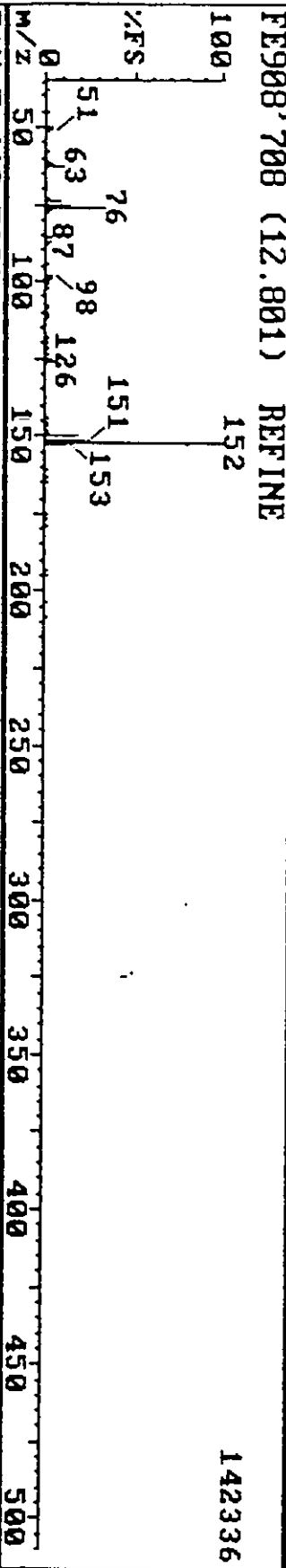
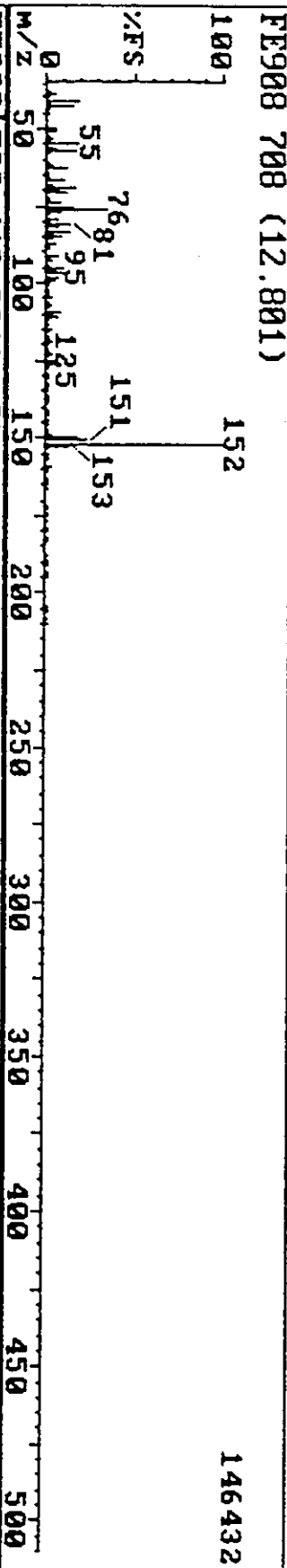


PAH 4 (10.684) 2-Methylnaphthalene

FIND 100



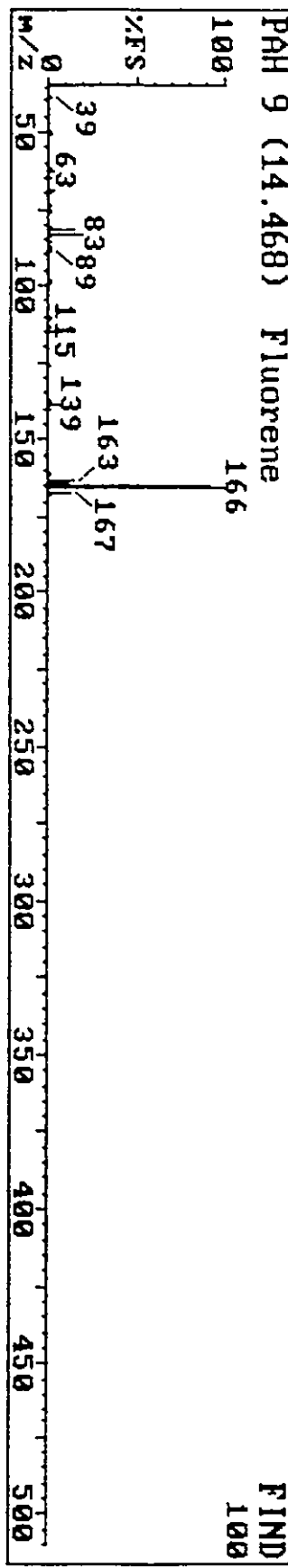
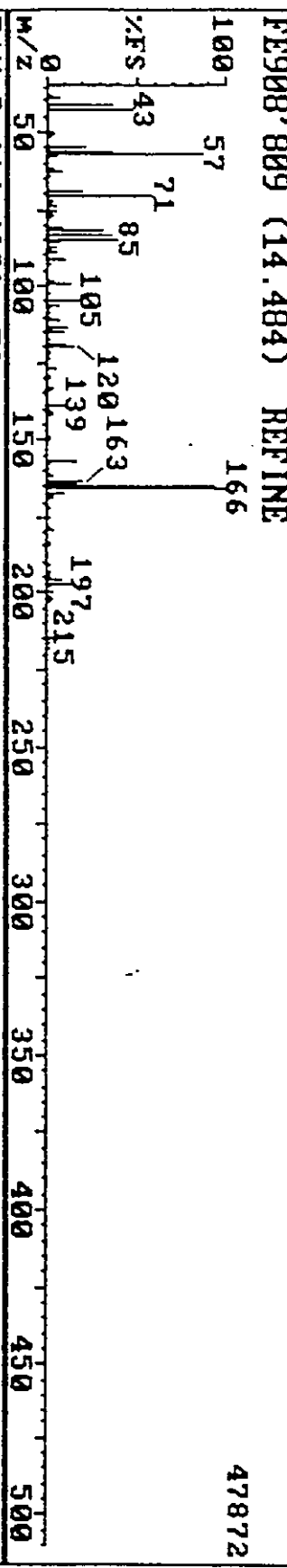
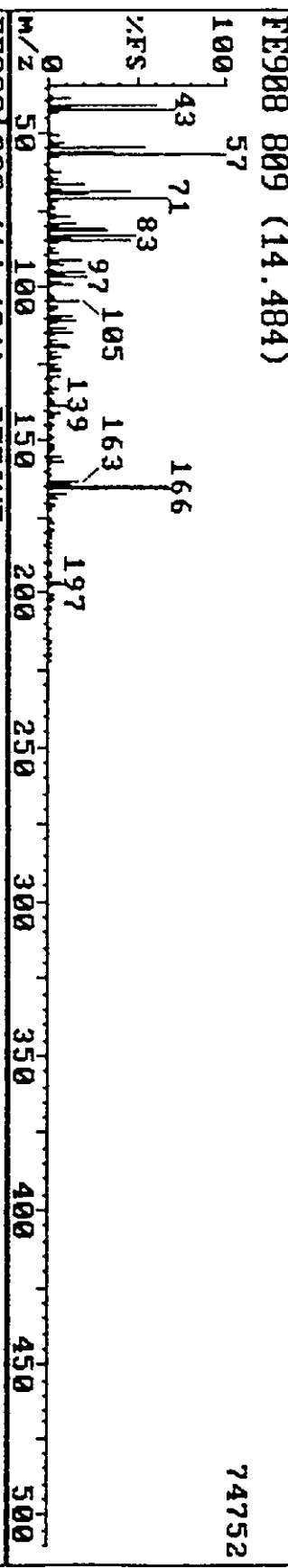
25-Sep-91 14:11 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#2 (1:2 DIL.) 18976 Instrument F



25-Sep-91 14:11
Sample: RUN#2 (1:2 DIL.)

Triangle Labs, Inc.
18976

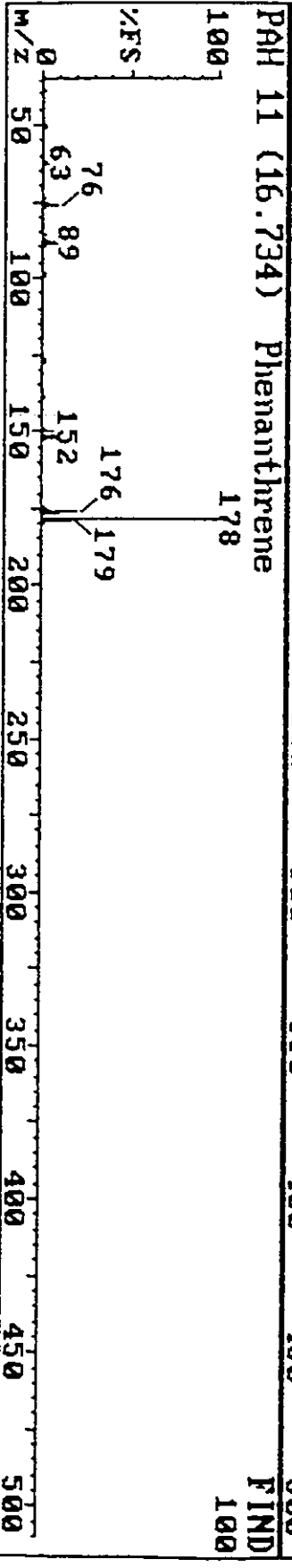
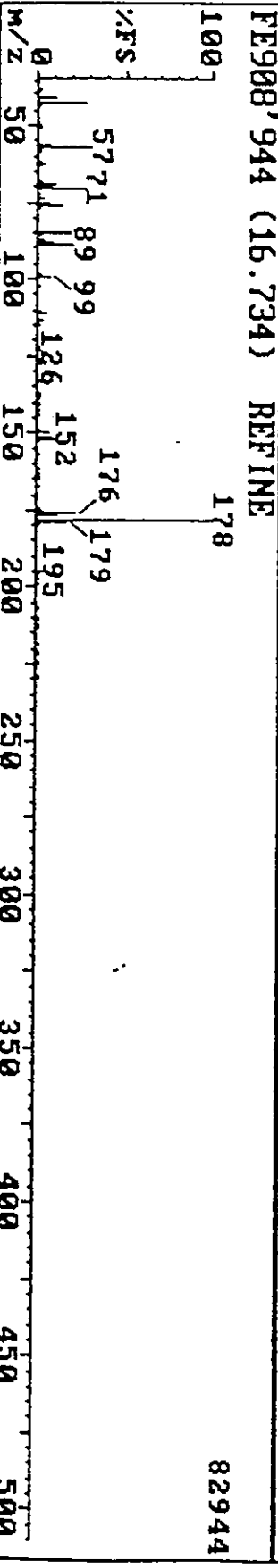
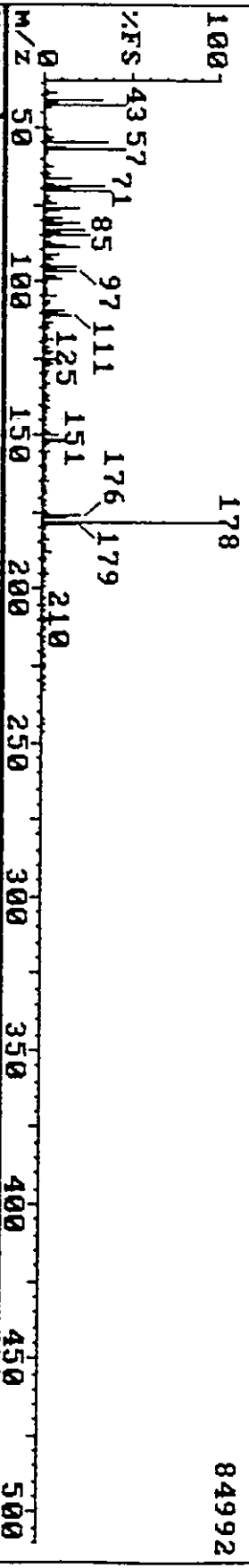
(919) 544-5729
Instrument F



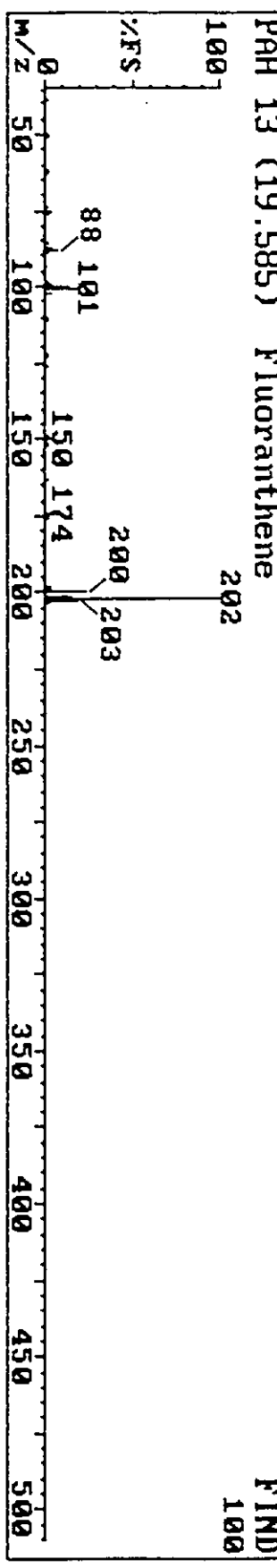
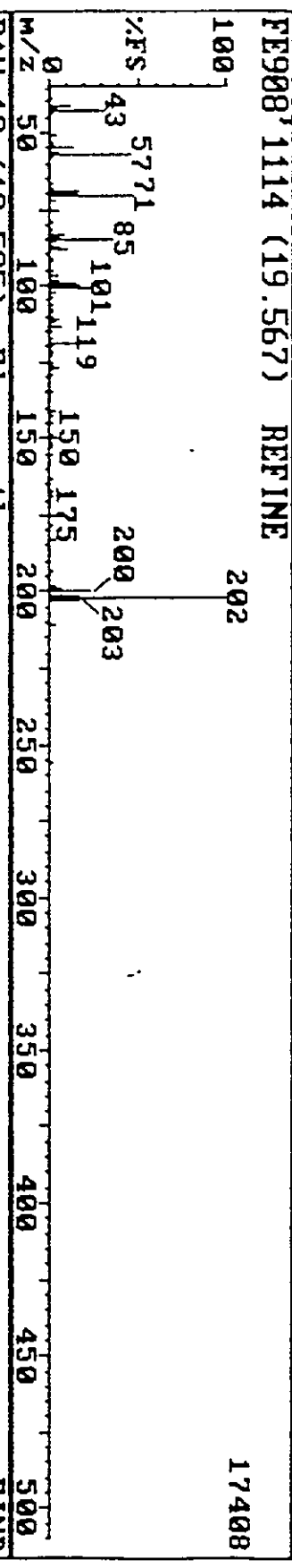
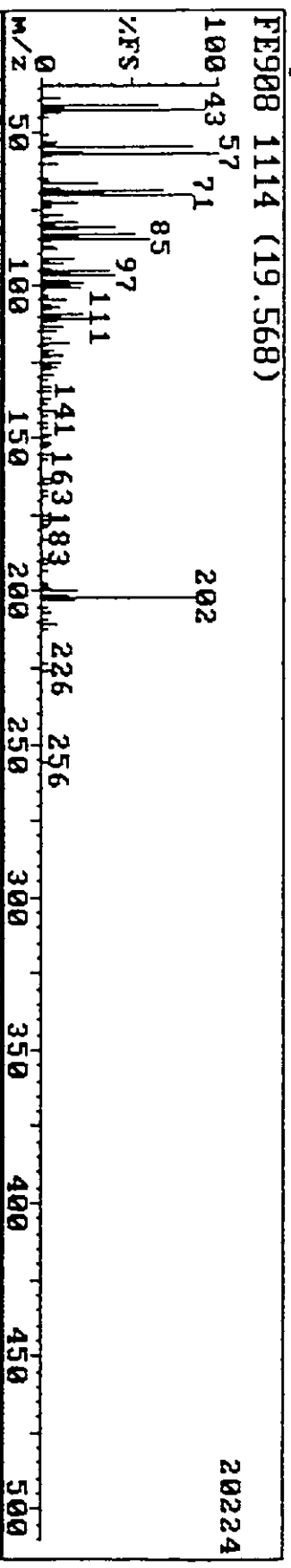
25-Sep-91 14:11 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#2 (1:2 DIL.) 18976 Instrument F

ju

FE908 944 (16.734) 84992



25-Sep-91 14:11 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#2 (1:2 DIL.) 18976 Instrument F



TRIANGLE LABORATORIES, INC.
 801 Capitoia Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE817
 RF FILE: FE807
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/19/91

SAMPLE ID: RUN #3
 DILN FACTOR: 1
 TLI Sample ID: 46.062.1A.H

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	1894		309	1		IS	
Naphthalene-d8	6598		484	14		IS	
Naphthalene	44416	.9104	487	14	295.77	D	10
2-Methylnaphthalene	16736	.7186	589	14	141.19	D	10
Acenaphthene-d10	4445		736	28		IS	
2-Chloronaphthalene	0	.9327	0	28	.19	ND	10
Acenaphthylene	14530	1.5120	715	28	86.47	D	10
Acenaphthene	0	1.0072	0	28	.18	ND	10
Fluorene	3982	.9405	817	28	38.20	D	10
Phenanthrene-d10	8251		950	47		IS	
Phenanthrene	4531	1.0774	953	47	20.39	D	10
Anthracene	668	1.0176	961	47	3.18	E	10
Fluoranthene	628	1.1700	1123	47	2.60	E	10
Chrysene-d12	9423		1338	57		IS	
Pyrene	0	.9377	0	57	.09	ND	10
Benzo(a)anthracene	0	1.0234	0	57	.08	ND	10
Chrysene	0	1.0396	0	57	.08	ND	10
Perylene-d12	10512		1557	64		IS	
Benzo(b)fluoranthene	0	.8831	0	64	.09	ND	10
Benzo(k)fluoranthene	0	.9783	0	64	.08	ND	10
Benzo(e)pyrene	0	.8487	0	64	.09	ND	10
Benzo(a)pyrene	0	.9448	0	64	.08	ND	10
Perylene	0	.5627	0	64	.14	ND	10
Indeno(1,2,3-cd)pyrene	0	.8595	0	64	.09	ND	10
Dibenz(a,h)anthracene	0	.9225	0	64	.08	ND	10
Benzo(g,h,i)perylene	0	.9620	0	64	.08	ND	10

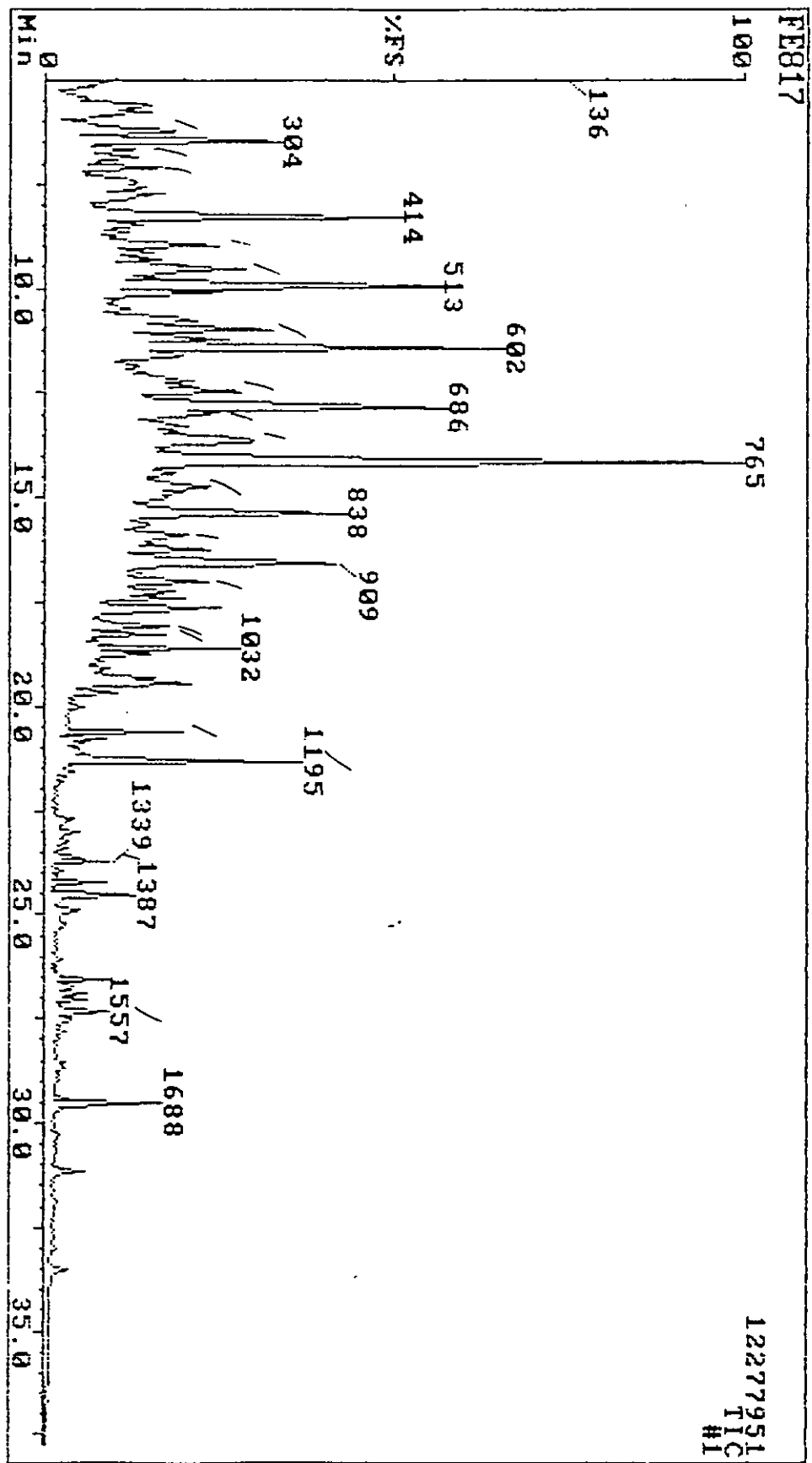
SURROGATE	SUMMARY	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14		19503	.6288	1195	57	131.66	D	131.7
Anthracene-d10		13748	.9242	959	47	72.12	D	72.1
Pyrene-d10		17738	.6547	1152	57	115.00	D	115.0
Phenol-d5		4095	1.1959	282	1	72.33	D	72.3
2,4,6-Tribromophenol		2083	.0779	853	28	240.57	D	240.6
1,4-Dibromobenzene-d4		2707	.4698	492	1	121.69	D	121.7

CODES: ND = Not Detected; D = Detected; E = Estimated; IS = Internal Standard

19-Sep-91 20:11
Sample: RUN#3 18976

Triangle Labs, Inc. ^{5nd}

(919) 544-5729
Instrument F



12277951
TIC
#1

N	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	47	31	86	5	189380	bv	309	152 1,4 Dichlorobenzene-d4
2	44	21	69	-3	659780	vv	484	136 Naphthalene-d8
3	96	70	96	1	4441600	bv	467	128 Naphthalene
4	84	50	84	0	1673600	vv	589	142 2-Methylnaphthalene
5	52	22	75	-2	444530	bv	736	164 Acenaphthene-d10
6	0	0	0	0	0		0	162 2-Chloronaphthalene
7	79	40	96	1	1453000	vv	715	152 Acenaphthylene
8	0	0	0	0	0		0	153 Acenaphthene
9	63	30	79	1	399220	vv	817	166 Fluorene
10	74	28	90	0	825060	vv	950	188 Phenanthrene-d10
11	67	23	93	0	453060	vv	953	178 Phenanthrene
12	56	11	79	0	66817	vv	961	178 Anthracene
13	42	15	79	-4	62784	vv	1123	202 Fluoranthene
14	58	69	93	-6	942330	bb	1338	240 Chrysene-d12
15	75	43	96	2	1930300	vb	1195	244 Terphenyl-d14
16	57	18	89	2	65990	bb	1154	202 Pyrene
17	0	0	0	0	0		0	228 Benzo(a)anthracene
18	0	0	0	0	0		0	228 Chrysene
19	92	67	92	1	1051200	bb	1557	264 Perylene-d12
20	0	0	0	0	0		0	252 Benzo(b)fluoranthene
21	0	0	0	0	0		0	252 Benzo(k)fluoranthene
22	0	0	0	0	0		0	252 Benzo(e)pyrene
23	0	0	0	0	0		0	252 Benzo(a)pyrene
24	0	0	0	0	0		0	252 Perylene
25	0	0	0	0	0		0	276 Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0		0	278 Dibenz(a,h)anthracene
27	0	0	0	0	0		0	276 Benzo(g,h,i)perylene
28	0	0	0	0	0		0	266 Pentachlorophenol
29	70	38	83	1	443490	vv	386	82 Nitrobenzene-d5
30	63	35	74	-1	867000	bv	648	172 2-Fluorobiphenyl
31	62	22	84	1	208270	bb	853	330 2,4,6-Tribromophenol
32	54	35	85	4	409530	vb	282	99 Phenol-d5
33	81	68	97	3	1773000	vb	1152	212 Pyrene-d10
34	85	51	96	1	1374800	vv	959	188 Anthracene-d10
35	54	20	90	-3	270660	bb	492	240 1,4-Dibromobenzene-d4
36	58	28	72	1	332290	bb	434	185 1,3,5-Trichlorobenzene-d3

19-Sep-91 20:11

Sample: RUMH3 18976

Triangle Labs, Inc.

(919) 544-5729

Sample: RUMH3

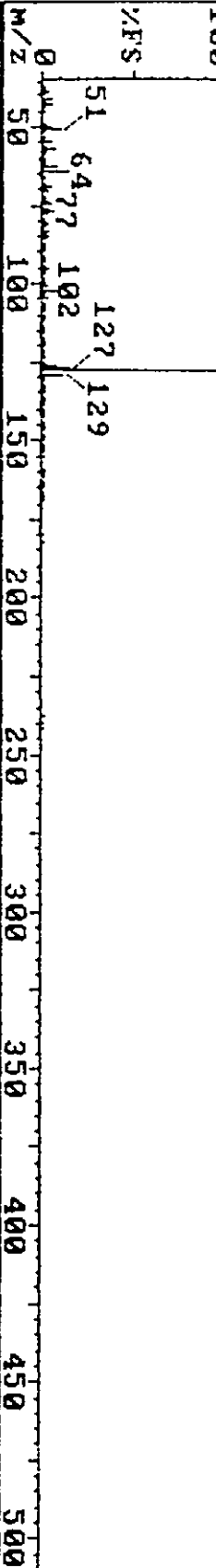
18976

Instrument F

FEB17 487 (9.517)

100 128

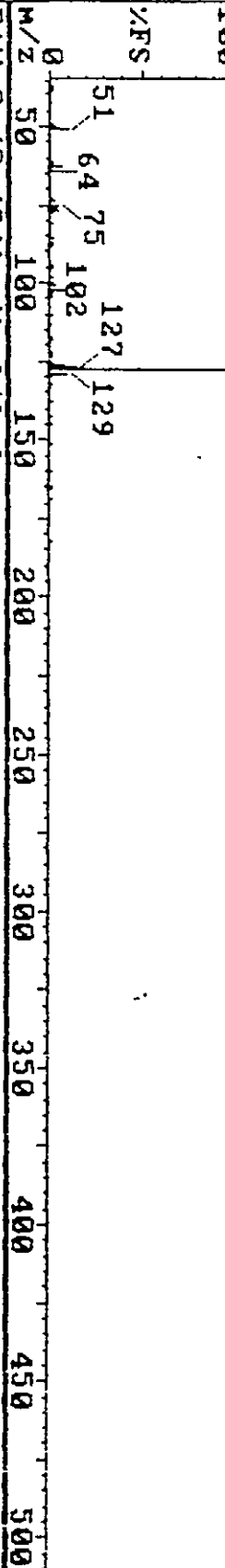
1081344



FEB17 487 (9.517) REFINE

100 128

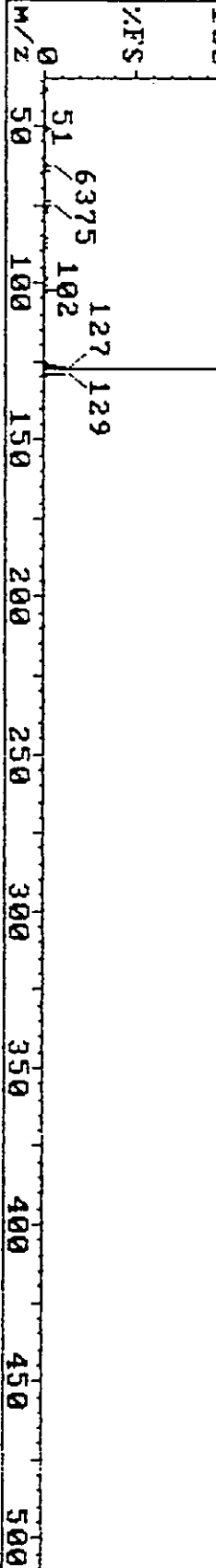
1064960



PAH 3 (9.434) Naphthalene

100 128

FIND 100



19-Sep-91 20:11

Sample: RUN#3 18976

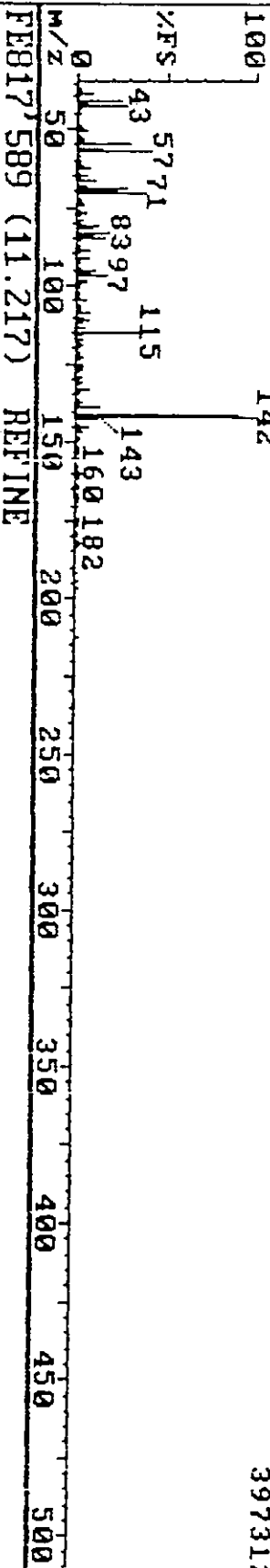
Triangle Labs, Inc.

(919) 544-5729
Instrument F

FEB17 589 (11.217)

142

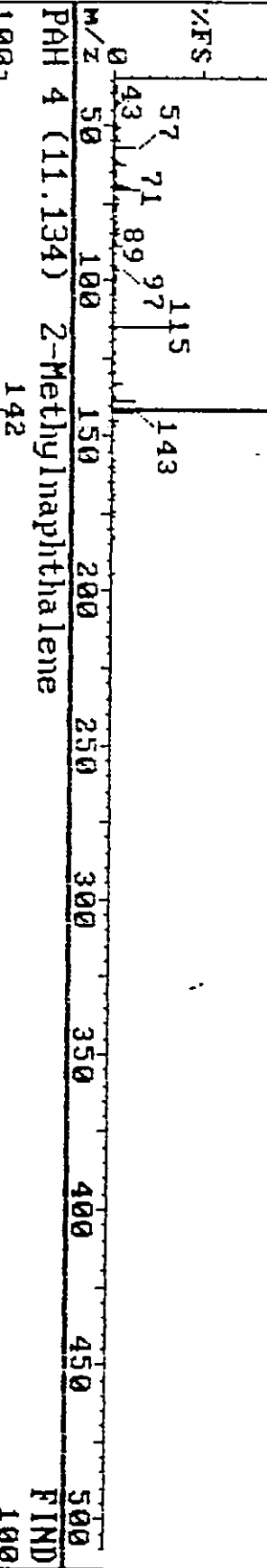
397312



FEB17 589 (11.217) REFINE

142

385024



PAH 4 (11.134) 2-Methylnaphthalene

142

FIND
100

19-Sep-91 20:11

Sample: RUN#3 18976

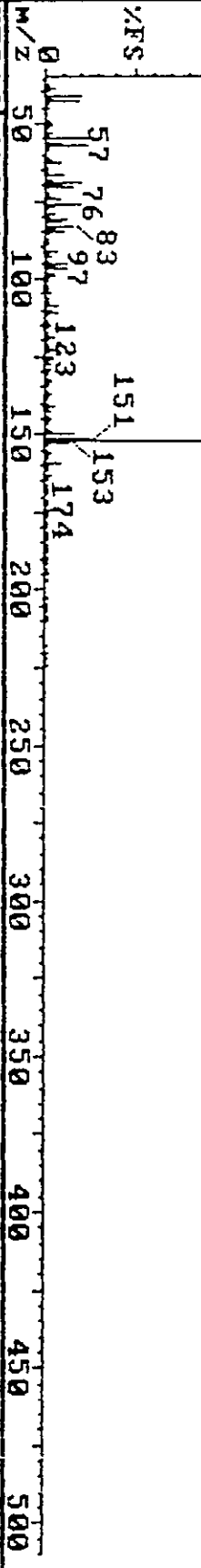
Triangle Labs, Inc.

(919) 544-5729
Instrument F

FEB17 715 (13.318)

152

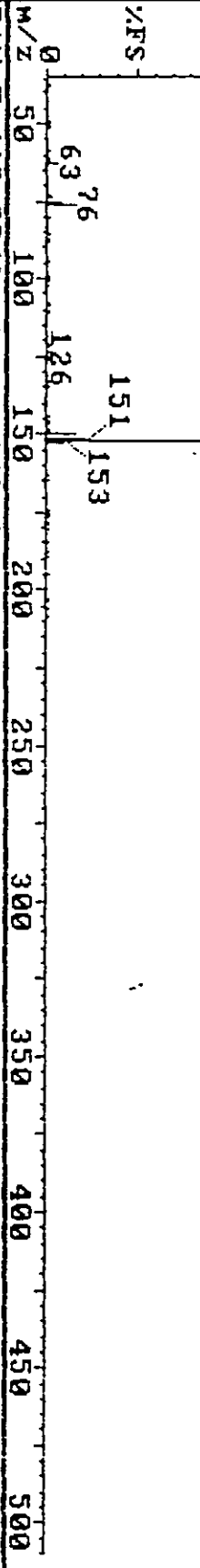
376832



FEB17 715 (13.317) REFINE

152

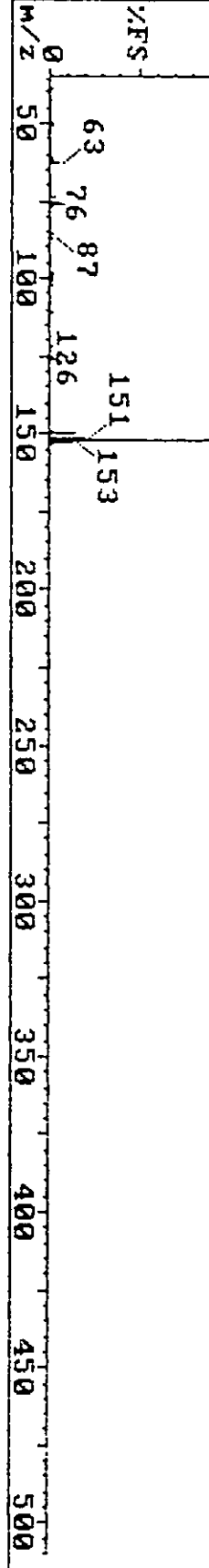
356352



PAH 7 (13.234) Acenaphthylene

152

FIND
100



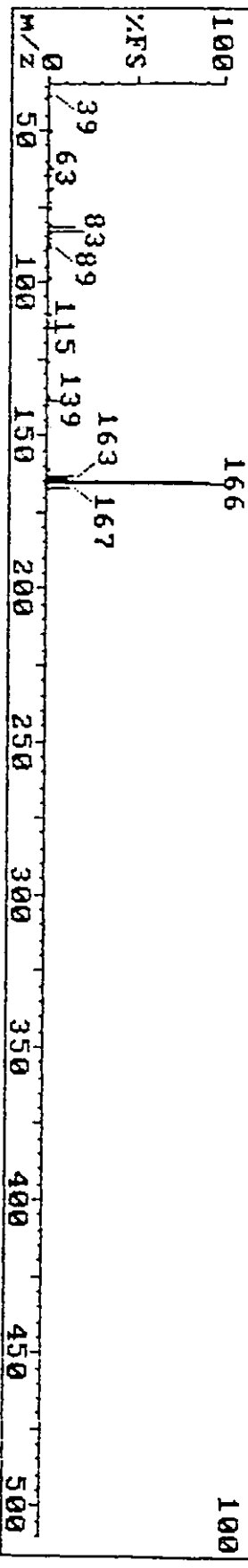
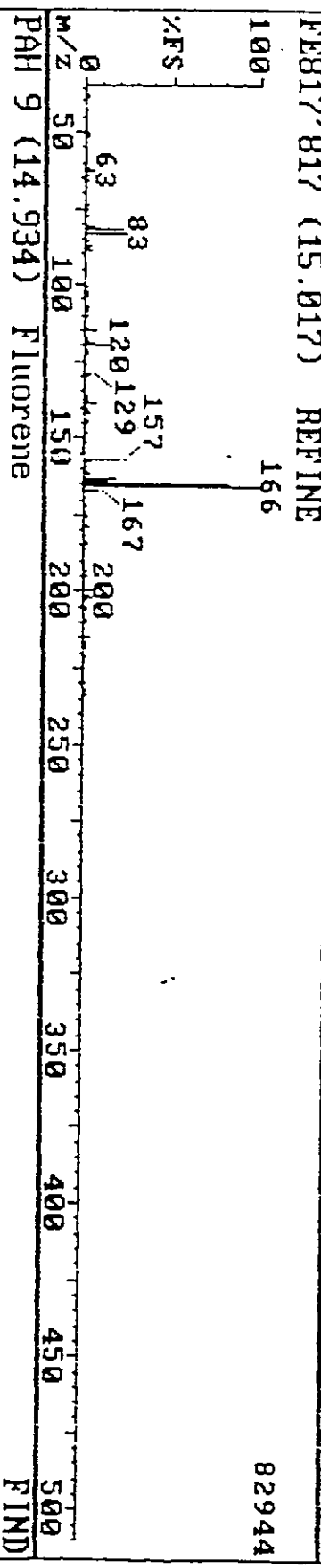
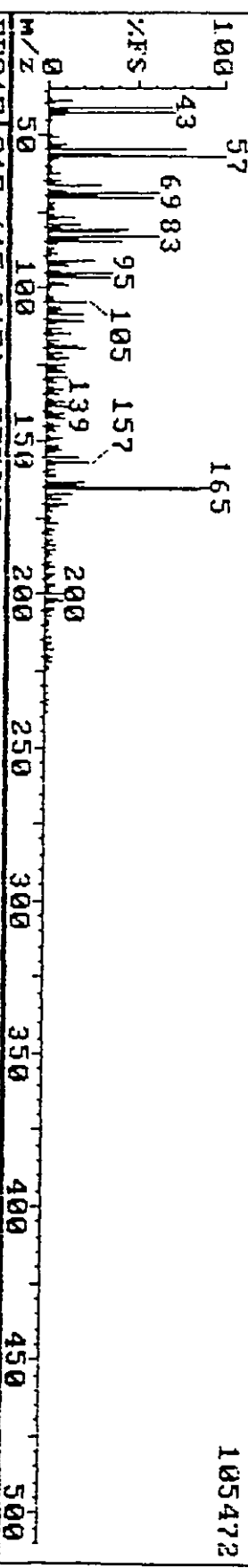
19-Sep-91 20:11

Sample: RUN#3 18976

Triangle Labs, Inc.

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Instrument F

FEB17 817 (15.018)



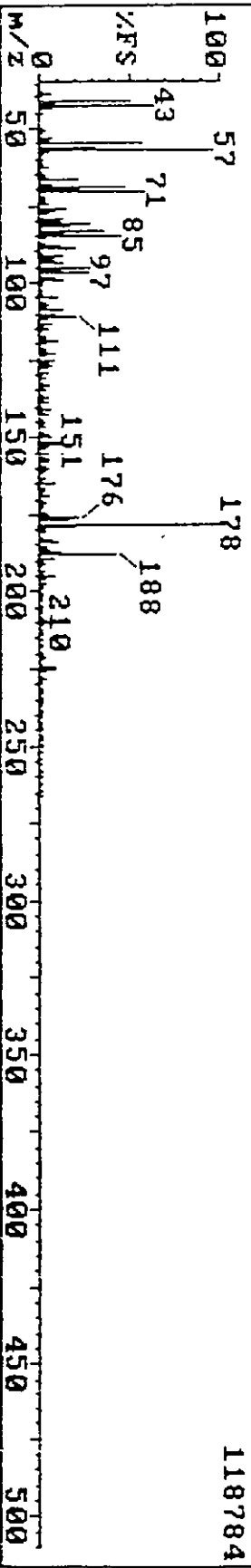
19-Sep-91 20:11

Sample: RUN#3 18976

Triangle Labs, Inc.

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Instrument F

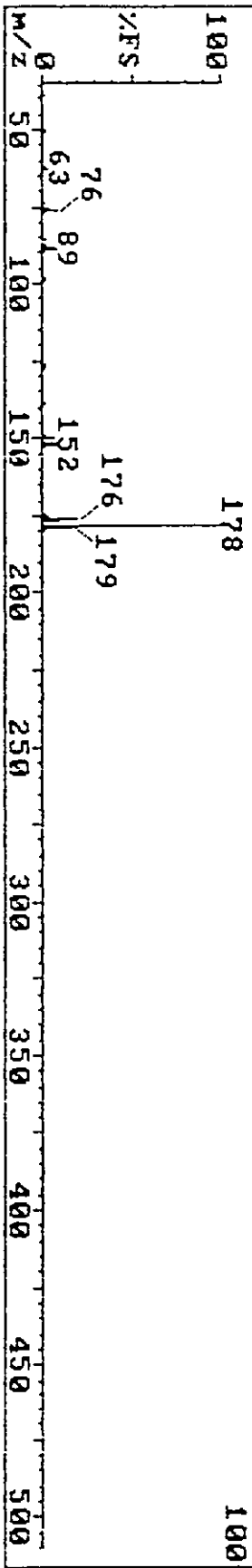
FEB17 953 (17.284)



FEB17 953 (17.284) REFINE

111616

PAH 11 (17.201) Phenanthrene



FIND
100

19-Sep-91 20:11

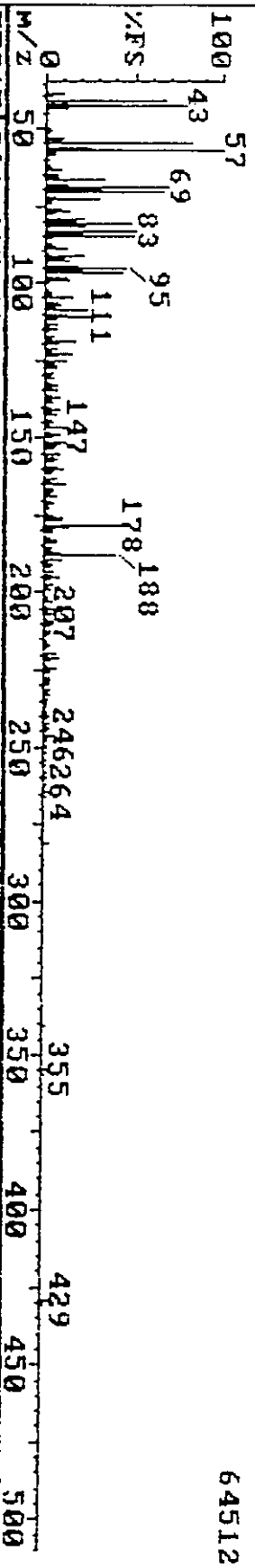
Sample: RUN#3 18976

Triangle Labs, Inc.

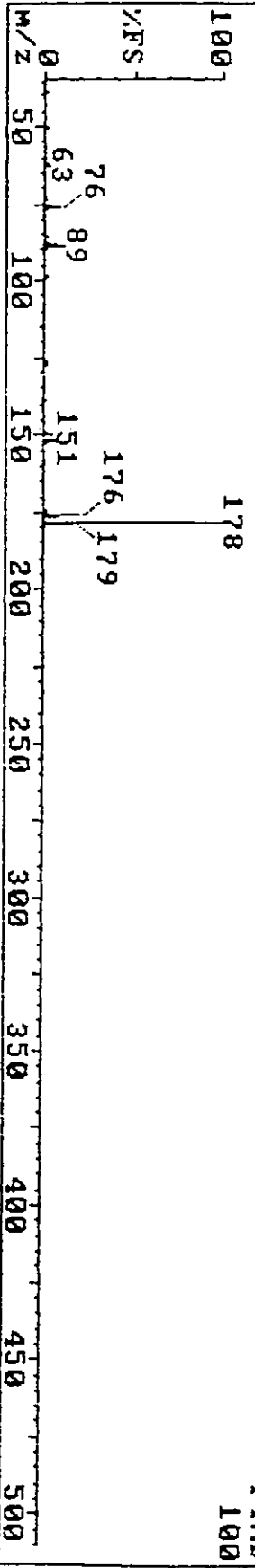
(919) 544-5729
Instrument F

3rd

FEB17 961 (17.418)



PAH 12 (17.334) Anthracene



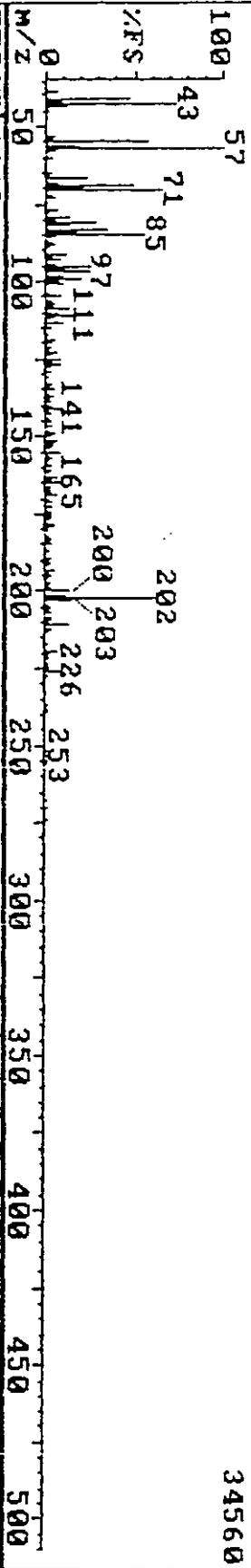
19-Sep-91 20:11

Sample: RUN#3 18976

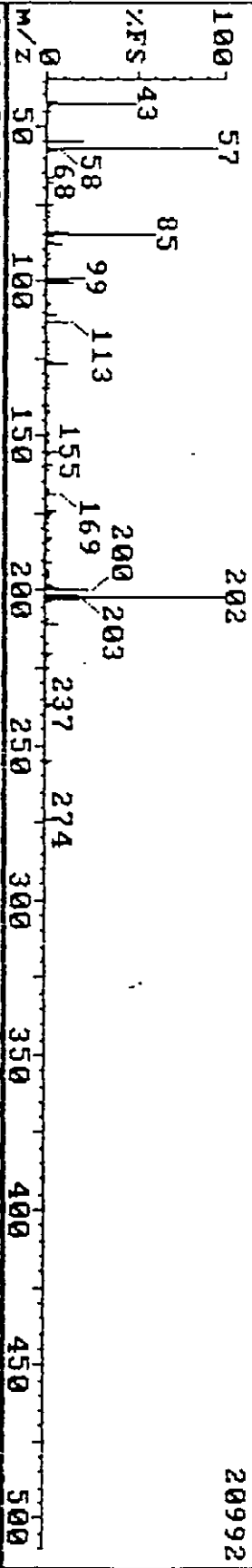
Triangle Labs, Inc.

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Instrument F

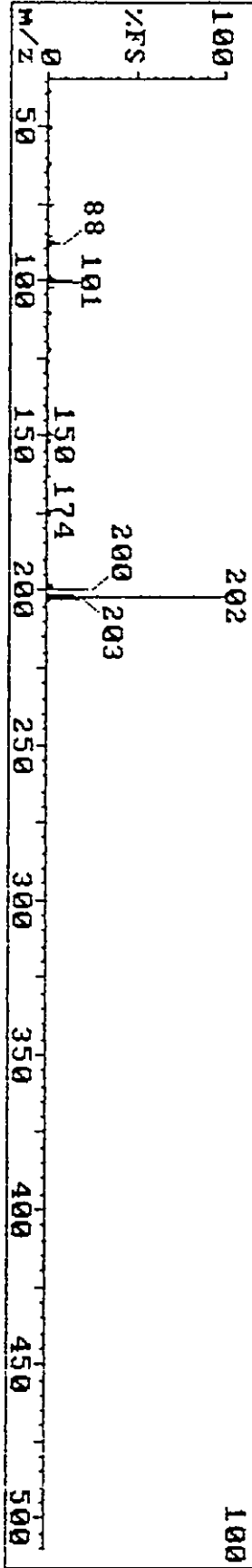
FE817 1123 (20.118)



FE817 1123 (20.117)



PAH 13 (20.085) Fluoranthene



TRIANGLE LABORATORIES, INC.
 801 Capitola Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE909
 RF FILE: FE901
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/25/91

SAMPLE ID: RUN #3 (1:4 dil.)
 DILN FACTOR: 4
 TLI Sample ID: 46.062.1A.H

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	911		303	1		IS	
Naphthalene-d8	3390		478	14		IS	
Naphthalene	6445	.9408	481	14	323.34	D	40
2-Methylnaphthalene	2133	.7942	582	14	126.79	D	40
Acenaphthene-d10	2112		729	28		IS	
2-Chloronaphthalene	0	.9237	0	28	1.64	ND	40
Acenaphthylene	2169	1.5395	707	28	106.71	D	40
Acenaphthene	0	.9778	0	28	1.55	ND	40
Fluorene	557	1.1415	808	28	36.98	E	40
Phenanthrene-d10	4543		941	47		IS	
Phenanthrene	713	.8666	943	47	28.97	E	40
Anthracene	0	.8724	0	47	.81	ND	40
Fluoranthene	118	1.3003	1113	47	3.20	E	40
Chrysene-d12	9935		1326	57		IS	
Pyrene	114	1.1620	1143	57	1.59	E	40
Benzo(a)anthracene	0	1.0992	0	57	.29	ND	40
Chrysene	0	1.0178	0	57	.32	ND	40
Perylene-d12	12078		1541	64		IS	
Benzo(b)fluoranthene	0	.9739	0	64	.27	ND	40
Benzo(k)fluoranthene	0	1.1928	0	64	.22	ND	40
Benzo(e)pyrene	0	.9749	0	64	.27	ND	40
Benzo(a)pyrene	0	1.0228	0	64	.26	ND	40
Perylene	0	.5802	0	64	.46	ND	40
Indeno(1,2,3-cd)pyrene	0	.8098	0	64	.33	ND	40
Dibenz(a,h)anthracene	0	.8430	0	64	.31	ND	40
Benzo(g,h,i)perylene	0	.9214	0	64	.29	ND	40

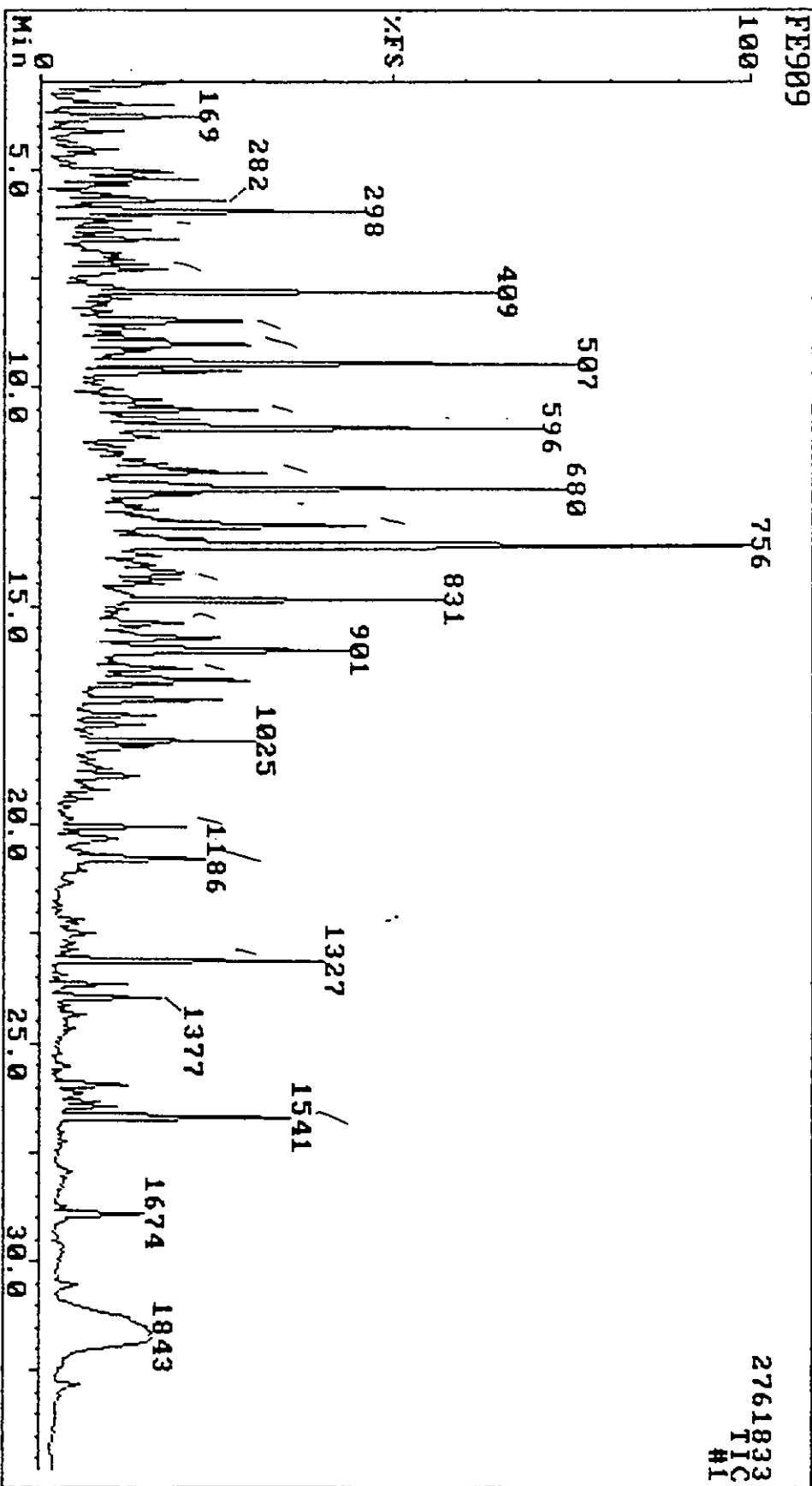
SURROGATE SUMMARY

	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14	3748	.8179	1186	57	73.81	D	73.8
Anthracene-d10	2131	.8804	948	47	85.27	D	85.3
Pyrene-d10	3382	.8714	1141	57	62.51	D	62.5
Phenol-d5	768	1.5876	274	1	84.98	D	85.0
2,4,6-Tribromophenol	259	.1108	843	28	177.14	D	177.1
1,4-Dibromobenzene-d4	377	.6186	486	1	107.05	D	107.1

25-Sep-91 14:55
Sample: RUN#3 (1:4 DIL.)

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18976

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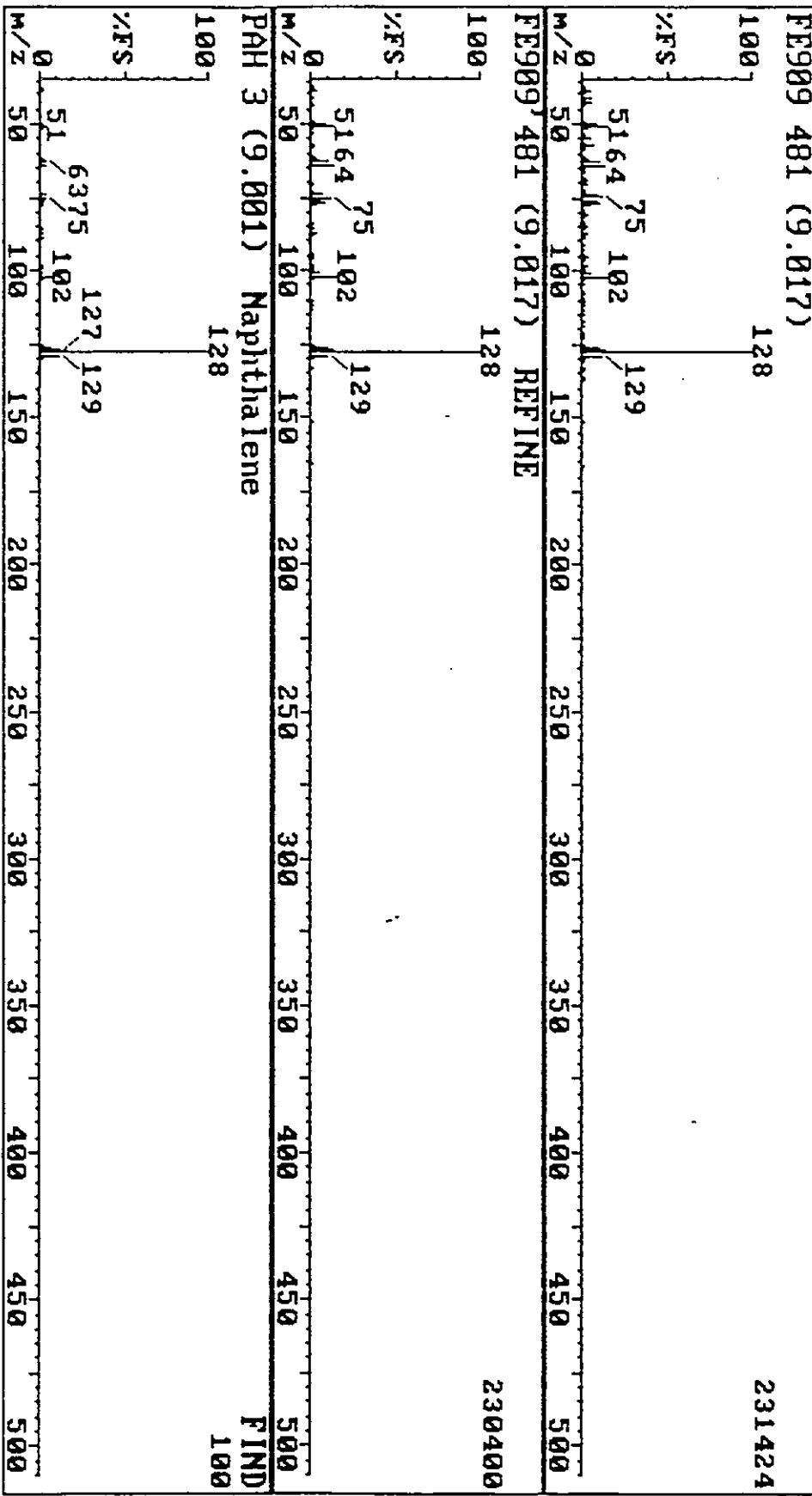
2761833
TIC
#1

I	MAT	FOR	REV	Delta	Area	F.Flags	Scan	QM	Name
1	89	58	96	1	91052	bb	303	152	1,4-Dichlorobenzene-d4
2	81	43	86	0	338980	bb	478	136	Naphthalene-d8
3	100	71	93	0	644510	bv	481	128	Naphthalene
4	89	56	87	0	213340	vb	582	142	2-Methylnaphthalene
5	81	42	88	0	211240	bb	729	164	Acenaphthene-d10
6	0	0	0	0	0		0	162	2-Chloronaphthalene
7	89	49	93	0	216900	vv	707	152	Acenaphthylene
8	0	0	0	0	0		0	153	Acenaphthene
9	60	28	76	-1	55740	vv	808	166	Fluorene
10	99	64	95	0	454270	vv	941	188	Phenanthrene-d10
11	63	26	91	-2	71272	vv	943	178	Phenanthrene
12	0	0	0	0	0		0	178	Anthracene
13	35	10	62	-3	11800	bb	1113	202	Fluoranthene
14	87	82	94	-3	993500	bb	1326	240	Chrysene-d12
15	86	63	97	2	374880	bb	1186	244	Terphenyl-d14
16	51	12	69	0	11440	bb	1143	202	Pyrene
17	0	0	0	0	0		0	228	Benzo(a)anthracene
18	0	0	0	0	0		0	228	Chrysene
19	92	79	92	2	1207800	bb	1541	264	Perylene-d12
20	0	0	0	0	0		0	252	Benzo(b)fluoranthene
21	0	0	0	0	0		0	252	Benzo(k)fluoranthene
22	0	0	0	0	0		0	252	Benzo(e)pyrene
23	0	0	0	0	0		0	252	Benzo(a)pyrene
24	0	0	0	0	0		0	252	Perylene
25	0	0	0	0	0		0	276	Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0		0	278	Dibenz(a,h)anthracene
27	0	0	0	0	0		0	276	Benzo(g,h,i)perylene
28	0	0	0	0	0		0	266	Pentachlorophenol
29	80	49	88	-1	121460	vv	381	82	Nitrobenzene-d5
30	64	37	74	-1	97820	bb	643	172	2-Fluorobiphenyl
31	61	30	64	-2	25912	bb	843	330	2,4,6-Tribromophenol
32	85	46	90	0	76776	bb	274	99	Phenol-d5
33	99	74	96	1	338220	bb	1141	212	Pyrene-d10
34	80	53	96	-2	213140	vb	948	188	Anthracene-d10
35	67	27	89	-1	37684	bb	486	240	1,4-Dibromobenzene-d4
36	67	35	72	0	36224	bb	428	185	1,3,5-Trichlorobenzene-d3

25-Sep-91 14:55
Sample: RUN#3 (1:4 DIL.)

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25-Sep-91 14:55

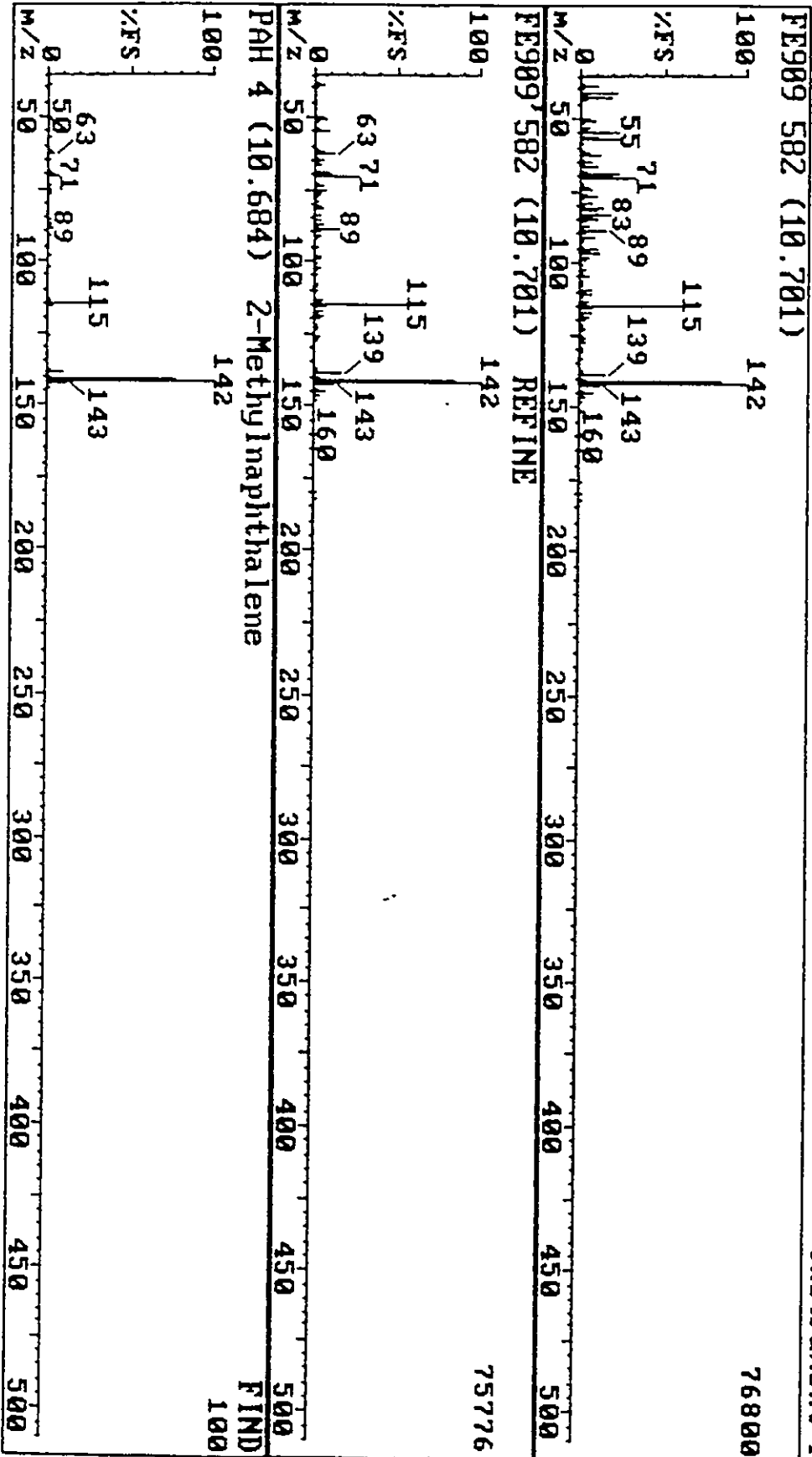
Triangle Labs, Inc.

(919) 544-5729

Sample: RUN#3 (1:4 DIL.)

18976

Instrument F



25-Sep-91 14:55

Triangle Labs, Inc.

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Sample: RUN#3 (1:4 DIL.)

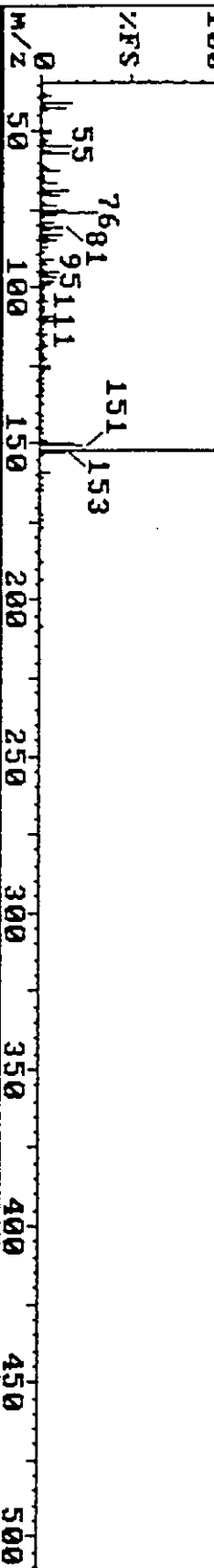
18976

Instrument F

FE909 707 (12.784)

152

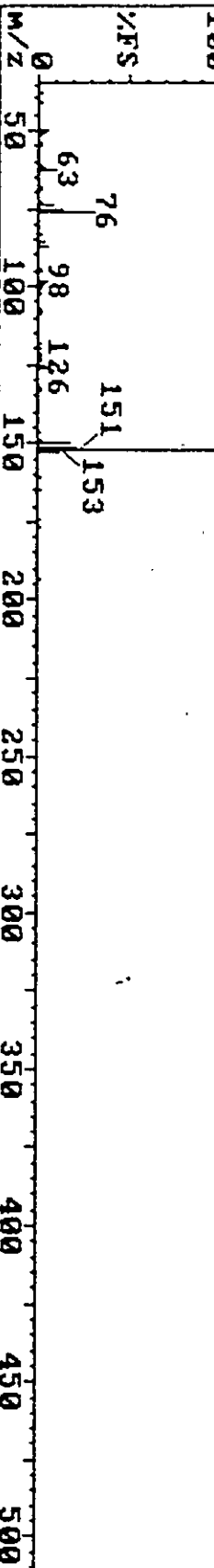
79872



FE909 707 (12.784) REFINE

152

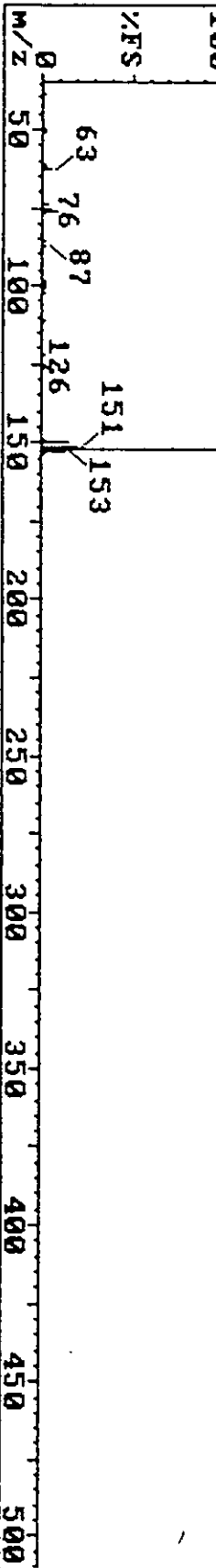
76800



PAH 7 (12.768) Acenaphthylene

152

FIND 100



25-Sep-91 14:55

Triangle Labs, Inc.

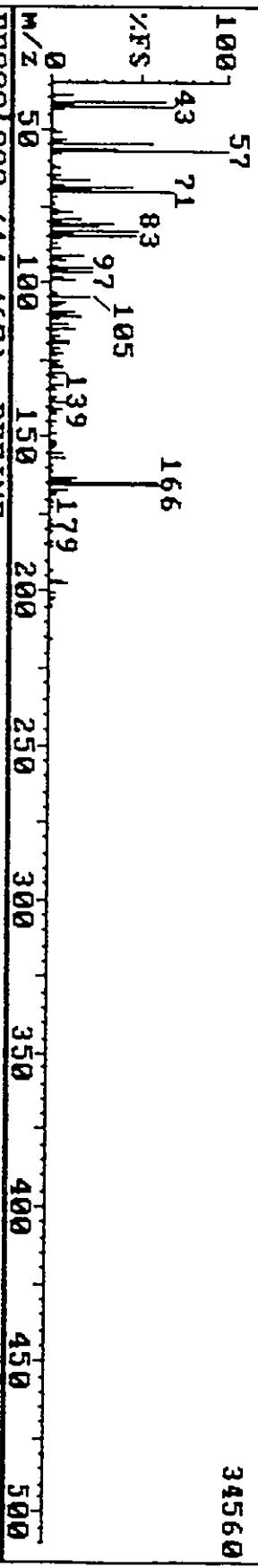
(919) 544-5729

Sample: RUN#3 (1:4 DIL.)

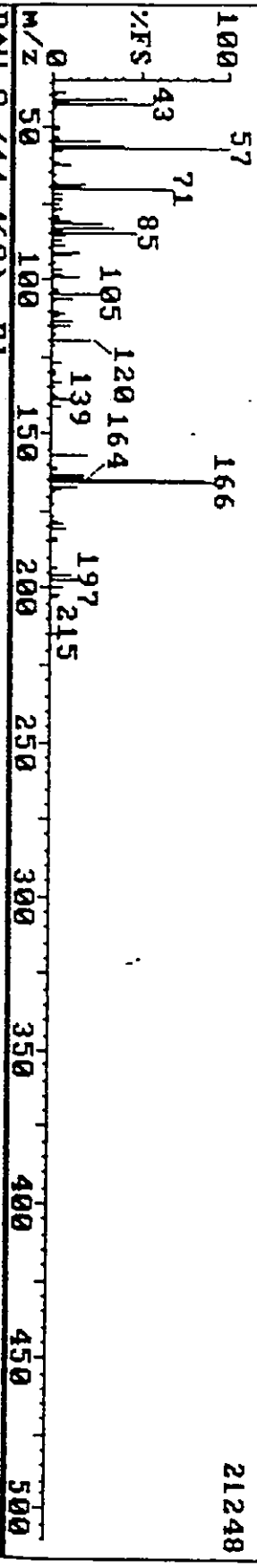
18976

Instrument F

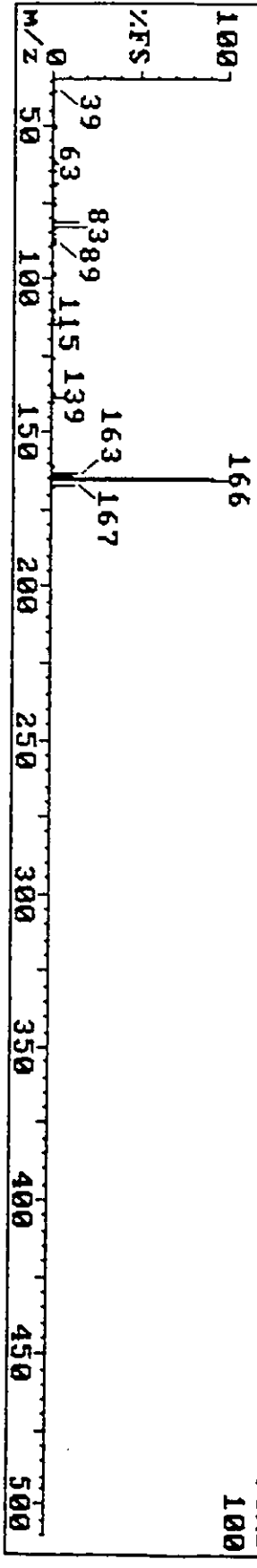
FE909 808 (14.468)



FE909 808 (14.467) REFINE



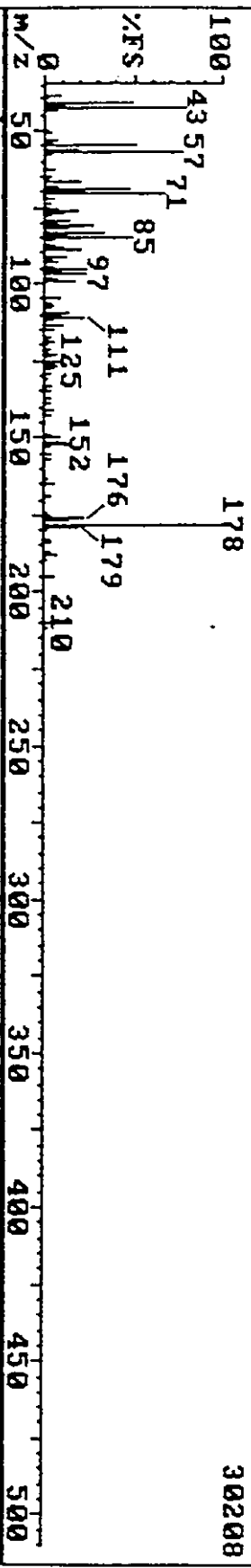
PAH 9 (14.468) Fluorene



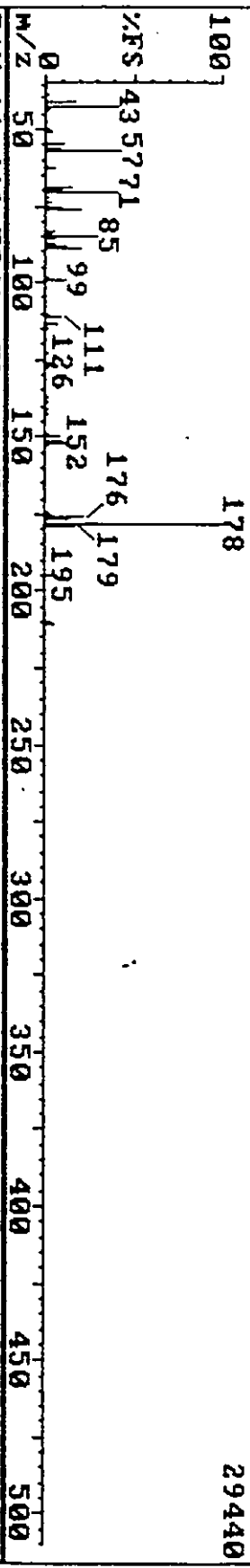
FIND
100

25-Sep-91 14:55 Triangle Labs, Inc. (919) 544-5729
Sample: RUN#3 (1:4 DIL.) 18976 Instrument F

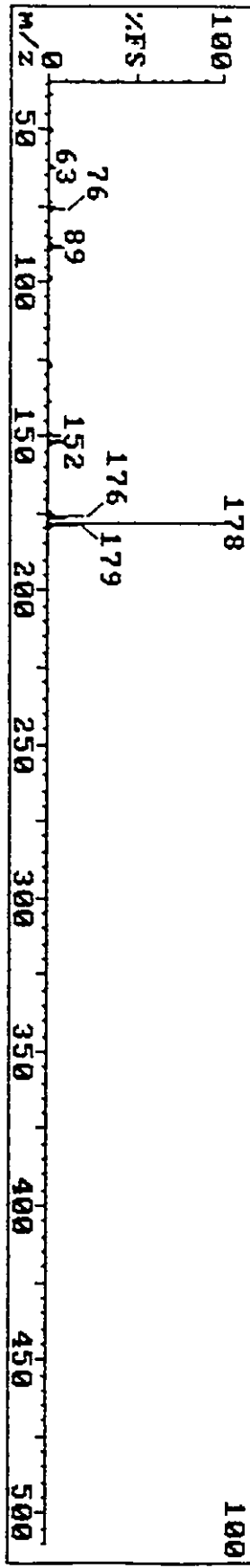
FE909 943 (16.718)



FE909 943 (16.717) REFINE



PAH 11 (16.734) Phenanthrene



FIND
100

29440

30208

25-Sep-91 14:55

Triangle Labs, Inc.

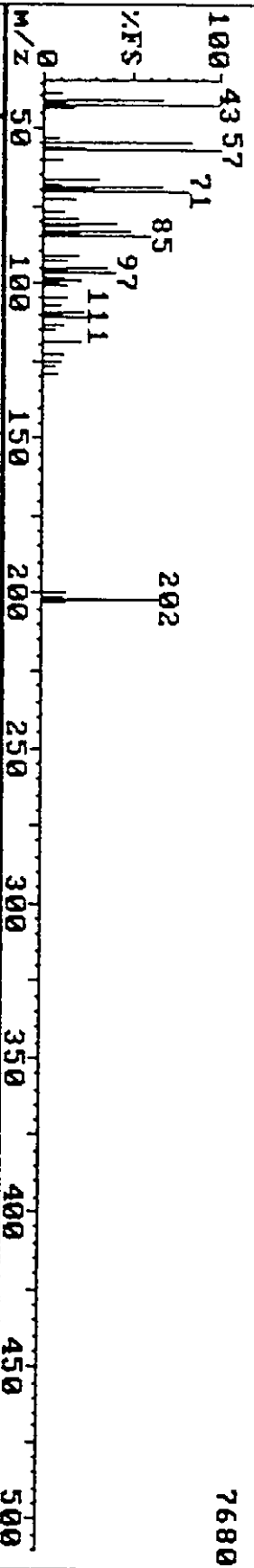
(919) 544-5729

Sample: RUN#3 (1:4 DIL.)

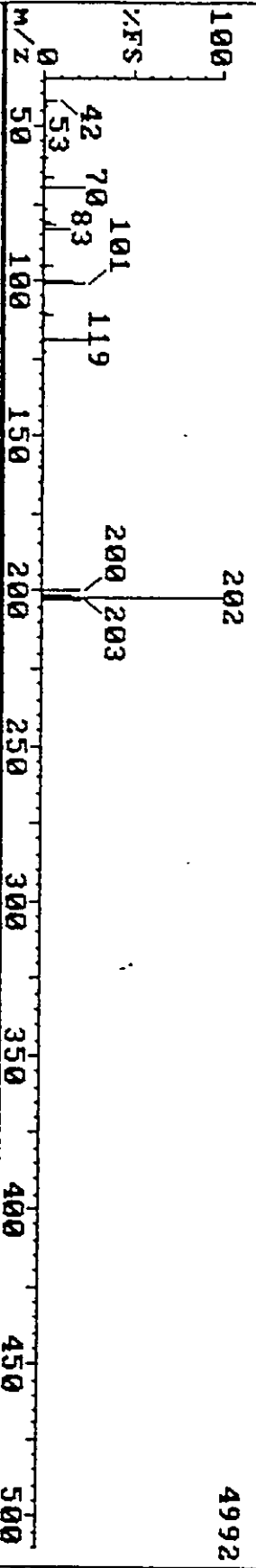
18976

Instrument F

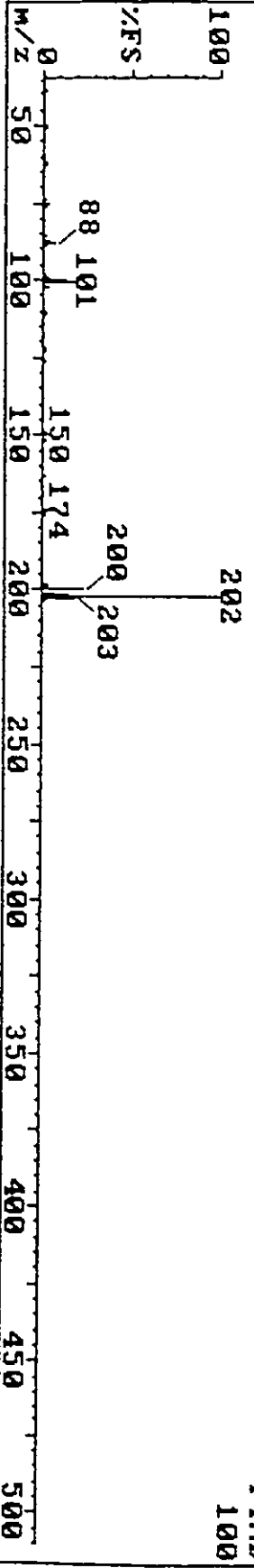
FE909 1113 (19.551)



FE909 1113 (19.551) REFINE



PAH 13 (19.585) Fluoranthene



FIND

100

4992

7680

25-Sep-91 14:55

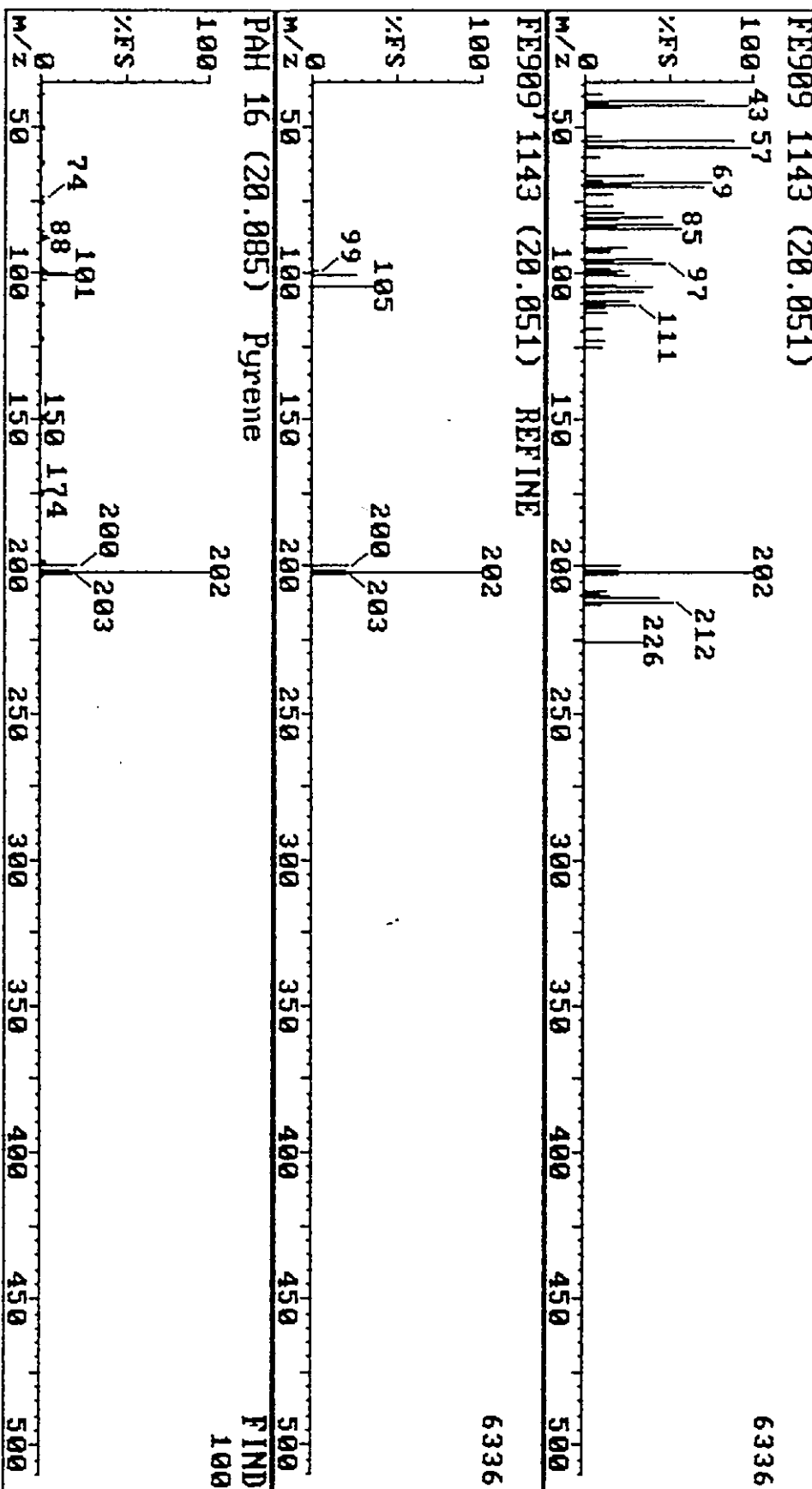
Triangle Labs, Inc.

(919) 544-5729

Sample: RUN#3 (1:4 DIL.)

18976

Instrument F



TRIANGLE LABORATORIES, INC.
 801 Capitola Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE818
 RF FILE: FE807
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/19/91

SAMPLE ID: XAD BLANK
 DILN FACTOR: 1
 TLI Sample ID: 46.062.2

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	1886		304	1		IS	
Naphthalene-d8	7998		479	14		IS	
Naphthalene	1661	.9104	482	14	9.13	E	10
2-Methylnaphthalene	0	.7186	0	14	.14	ND	10
Acenaphthene-d10	5436		732	28		IS	
2-Chloronaphthalene	0	.9327	0	28	.16	ND	10
Acenaphthylene	0	1.5120	0	28	.10	ND	10
Acenaphthene	0	1.0072	0	28	.15	ND	10
Fluorene	0	.9405	0	28	.16	ND	10
Phenanthrene-d10	9857		945	47		IS	
Phenanthrene	60	1.0774	948	47	.23	E	10
Anthracene	0	1.0176	0	47	.08	ND	10
Fluoranthene	0	1.1700	0	47	.07	ND	10
Chrysene-d12	13219		1337	57		IS	
Pyrene	0	.9377	0	57	.06	ND	10
Benzo(a)anthracene	0	1.0234	0	57	.06	ND	10
Chrysene	0	1.0396	0	57	.06	ND	10
Perylene-d12	13388		1555	64		IS	
Benzo(b)fluoranthene	0	.8831	0	64	.07	ND	10
Benzo(k)fluoranthene	0	.9783	0	64	.06	ND	10
Benzo(e)pyrene	0	.8487	0	64	.07	ND	10
Benzo(a)pyrene	0	.9448	0	64	.06	ND	10
Perylene	0	.5627	0	64	.11	ND	10
Indeno(1,2,3-cd)pyrene	0	.8595	0	64	.07	ND	10
Dibenz(a,h)anthracene	0	.9225	0	64	.06	ND	10
Benzo(g,h,i)perylene	0	.9620	0	64	.06	ND	10

SURROGATE	SUMMARY	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14		21282	.6288	1193	57	102.42	D	102.4
Anthracene-d10		9857	.9242	945	47	43.28	D	43.3
Pyrene-d10		22909	.6547	1149	57	105.89	D	105.9
Phenol-d5		1988	1.1959	273	1	35.25	D	35.3
2,4,6-Tribromophenol		1696	.0779	847	28	160.19	D	160.2
1,4-Dibromobenzene-d4		1306	.4698	487	1	58.96	D	59.0

CODES: ND = Not Detected; D = Detected; E = Estimated; IS = Internal Standard

19-Sep-91 20:59

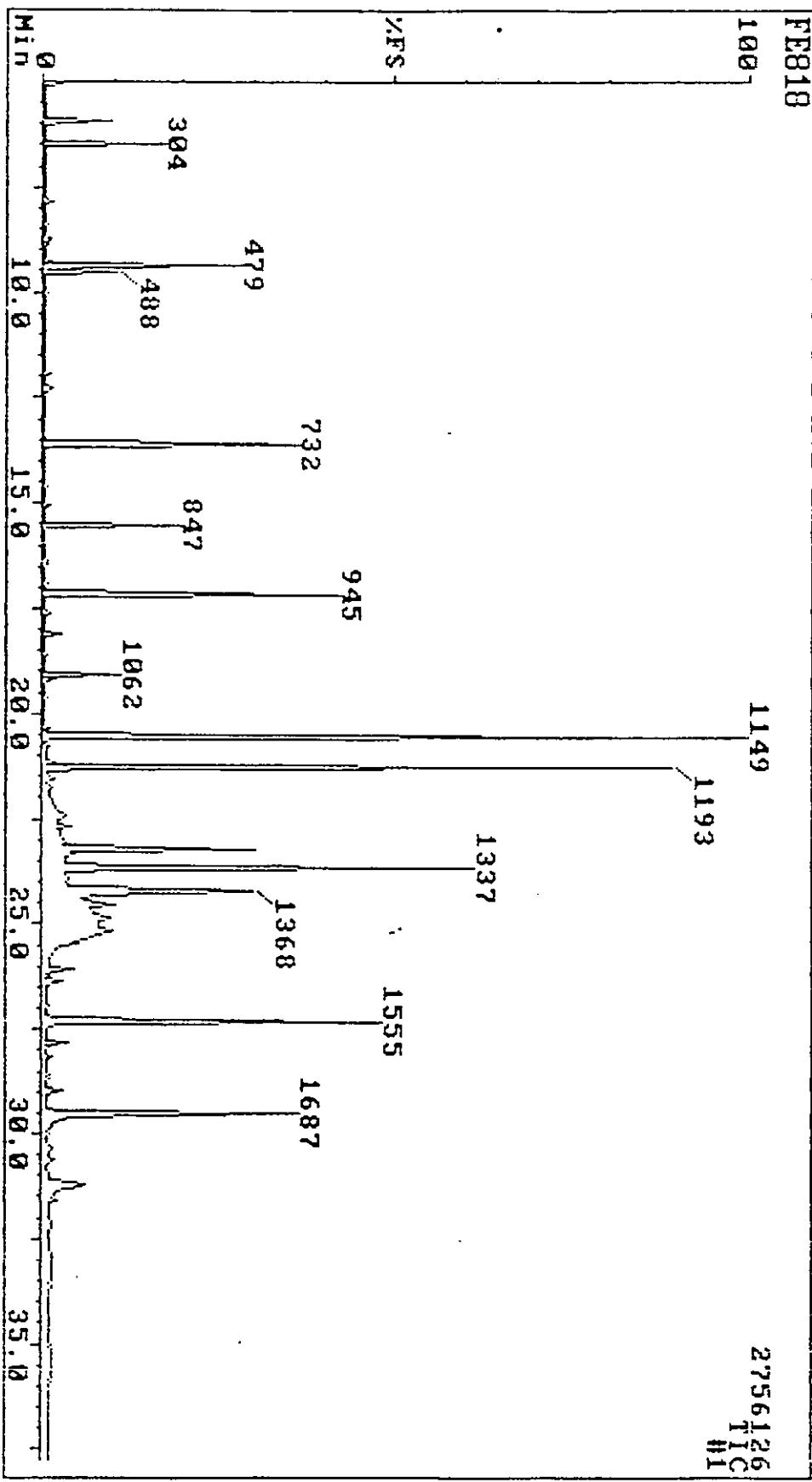
Sample: XAD BLANK

18976

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Instrument F



QUAN DB : FE818

LAB-BASE QUAN

19-Sep-91

23:04

	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM	Name
1	100	87	98	0	188600	bb	304	152	1,4-Dichlorobenzene-d4
2	100	89	92	-1	799620	bb	479	136	Naphthalene-d8
3	100	83	95	1	166080	bb	482	128	Naphthalene
4	48	19	64	1	543630	bb	584	142	2-Methylnaphthalene
5	100	97	99	1	543630	bb	732	164	Acenaphthene-d10
6	0	0	0	0	0		0	162	2-Chloronaphthalene
7	0	0	0	0	0		0	152	Acenaphthylene
8	0	0	0	0	0		0	153	Acenaphthene
9	0	0	0	0	0		0	166	Fluorene
10	100	93	97	0	985650	bv	945	188	Phenanthrene-d10
11	48	16	60	0	6048	bb	948	178	Phenanthrene
12	21	16	62	-8	6048	bb	948	178	Anthracene
13	0	0	0	0	0		0	202	Fluoranthene
14	100	83	93	0	1321900	bb	1337	240	Chrysene-d12
15	100	89	98	1	2128200	vb	1193	244	Terphenyl-d14
16	0	0	0	0	0		0	202	Pyrene
17	0	0	0	0	0		0	228	Benzo(a)anthracene
18	0	0	0	0	0		0	228	Chrysene
19	100	88	92	0	1338800	bb	1555	264	Perylene-d12
20	0	0	0	0	0		0	252	Benzo(b)fluoranthene
21	0	0	0	0	0		0	252	Benzo(k)fluoranthene
22	0	0	0	0	0		0	252	Benzo(e)pyrene
23	0	0	0	0	0		0	252	Benzo(a)pyrene
24	0	0	0	0	0		0	252	Perylene
25	0	0	0	0	0		0	276	Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0		0	278	Dibenz(a,h)anthracene
27	0	0	0	0	0		0	276	Benzo(g,h,i)perylene
28	0	0	0	0	0		0	266	Pentachlorophenol
29	0	0	0	0	0		0	82	Nitrobenzene-d5
30	0	0	0	0	0		0	172	2-Fluorobiphenyl
31	95	71	81	0	169610	bb	847	330	2,4,6-Tribromophenol
32	100	91	97	0	198790	bb	273	99	Phenol-d5
33	100	89	96	1	2290900	bb	1149	212	Pyrene-d10
34	51	92	97	-8	985650	bv	945	188	Anthracene-d10
35	100	94	96	-1	130580	bb	487	240	1,4-Dibromobenzene-d4
36	0	0	0	0	0		0	185	1,3,5-Trichlorobenzene-d3

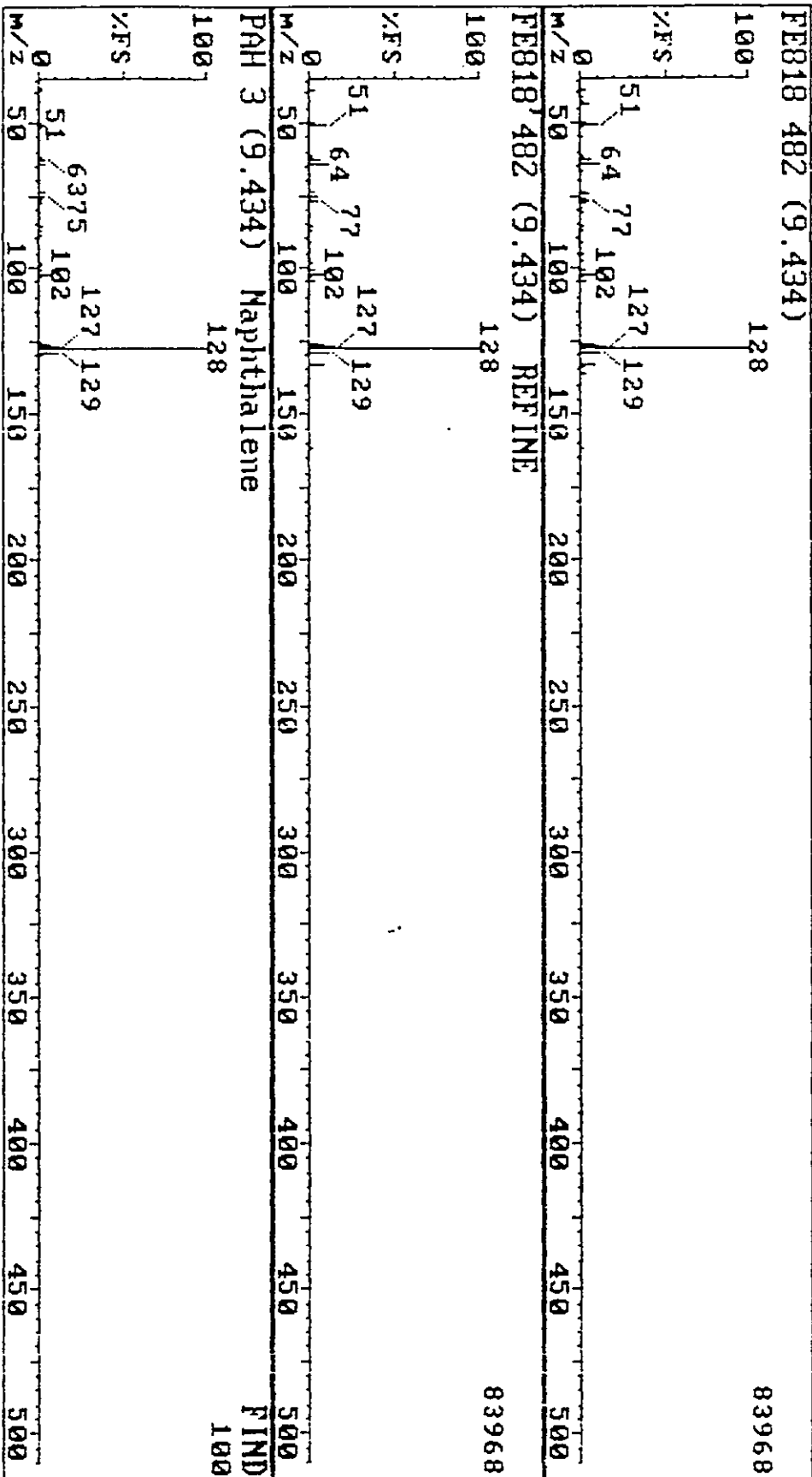
19-Sep-91 20:59

Sample: XAD BLANK 18976

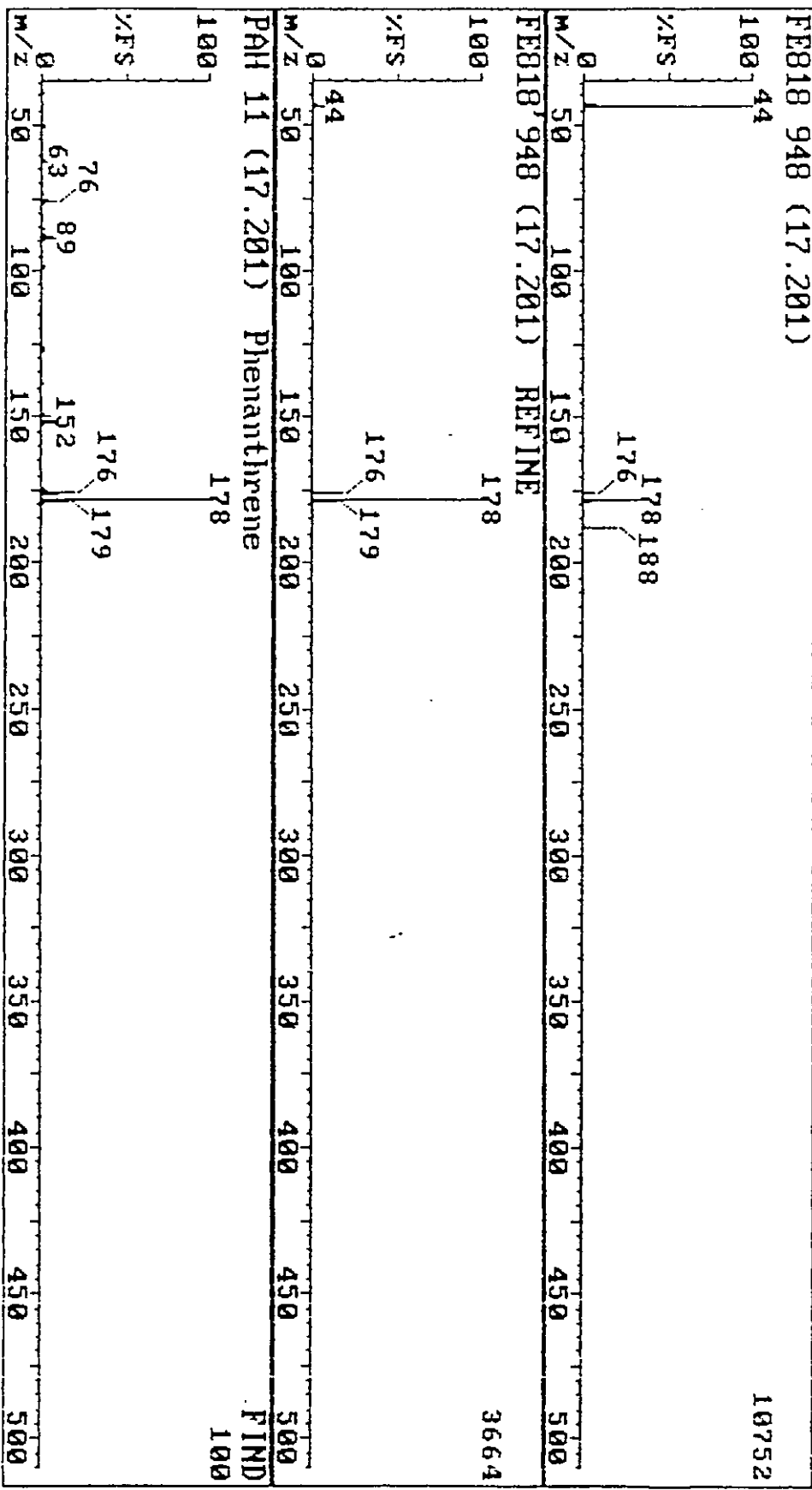
Triangle Labs, Inc.

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Instrument F

CMV



19-Sep-91 20:59
Sample: XAD BLANK
18976
Triangle Labs, Inc.
(919) 544-5729
Instrument F



TRIANGLE LABORATORIES, INC.
 801 Capitoia Drive
 Durham, NC 27713
 Telephone: (919) 544-5729

DATA FILE: FE814
 RF FILE: FE807
 DATE: 09/30/91
 TLI Project Number: 18976
 ANALYSIS DATE: 09/19/91

SAMPLE ID: SBLK 091991
 DILN FACTOR: 1
 TLI Sample ID:

QUANTITATION REPORT

NAME	AREA	RF	SCAN	ISID	AMOUNT, ug	CODE	QUAN LIMIT
1,4-Dichlorobenzene-d4	1040		304	1		IS	
Naphthalene-d8	4104		479	14		IS	
Naphthalene	1905	.9104	482	14	20.39	D	10
2-Methylnaphthalene	0	.7186	0	14	.27	ND	10
Acenaphthene-d10	2302		731	28		IS	
2-Chloronaphthalene	0	.9327	0	28	.37	ND	10
Acenaphthylene	0	1.5120	0	28	.23	ND	10
Acenaphthene	0	1.0072	0	28	.35	ND	10
Fluorene	0	.9405	0	28	.37	ND	10
Phenanthrene-d10	2594		945	47		IS	
Phenanthrene	0	1.0774	0	47	.29	ND	10
Anthracene	0	1.0176	0	47	.30	ND	10
Fluoranthene	0	1.1700	0	47	.26	ND	10
Chrysene-d12	2805		1335	57		IS	
Pyrene	0	.9377	0	57	.30	ND	10
Benzo(a)anthracene	0	1.0234	0	57	.28	ND	10
Chrysene	0	1.0396	0	57	.27	ND	10
Perylene-d12	3560		1554	64		IS	
Benzo(b)fluoranthene	0	.8831	0	64	.25	ND	10
Benzo(k)fluoranthene	0	.9783	0	64	.23	ND	10
Benzo(e)pyrene	0	.8487	0	64	.26	ND	10
Benzo(a)pyrene	0	.9448	0	64	.24	ND	10
Perylene	0	.5627	0	64	.40	ND	10
Indeno(1,2,3-cd)pyrene	0	.8595	0	64	.26	ND	10
Dibenz(a,h)anthracene	0	.9225	0	64	.24	ND	10
Benzo(g,h,i)perylene	0	.9620	0	64	.23	ND	10

SURROGATE	SUMMARY	AREA	RF	SCAN	ISID	AMOUNT	CODE	% RECOVERY
Terphenyl-d14		4237	.6288	1192	57	96.09	D	96.1
Anthracene-d10		4932	.9242	953	47	82.30	D	82.3
Pyrene-d10		4614	.6547	1148	57	100.51	D	100.5
Phenol-d5		1718	1.1959	272	1	55.27	D	55.3
2,4,6-Tribromophenol		250	.0779	846	28	55.72	D	55.7
1,4-Dibromobenzene-d4		671	.4698	487	1	54.94	D	54.9

CODES: ND = Not Detected; D = Detected; E = Estimated; IS = Internal Standard

19-Sep-91 17:48

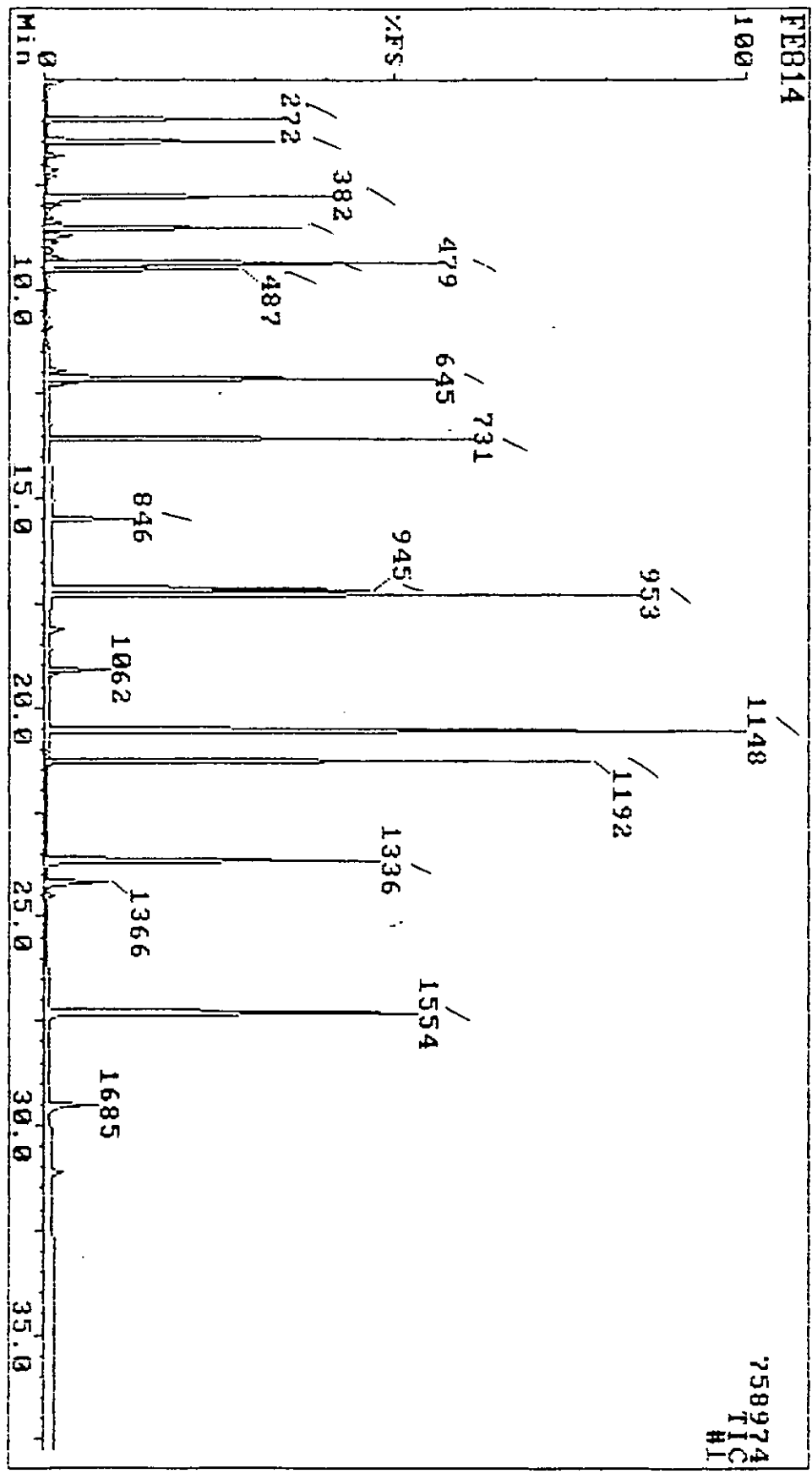
Sample: SBLK 091291

18976

Triangle Labs, Inc.

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Instrument F



QUAN DB : FEB14

JM
LAB-BASE QUAN

19-Sep-91

22:54

N	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	90	99	0	103950	bb	304	152 1,4 Dichlorobenzene-d4
2	100	93	96	-1	410370	bb	479	136 Naphthalene-d8
3	100	87	96	1	190460	bb	482	128 Naphthalene
4	0	0	0	0	0		0	142 2-Methylnaphthalene
5	100	98	99	0	230160	bb	731	164 Acenaphthene-d10
6	0	0	0	0	0		0	162 2-Chloronaphthalene
7	0	0	0	0	0		0	152 Acenaphthylene
8	0	0	0	0	0		0	153 Acenaphthene
9	0	0	0	0	0		0	166 Fluorene
10	100	94	97	1	259370	bv	945	188 Phenanthrene-d10
11	0	0	0	0	0		0	178 Phenanthrene
12	0	0	0	0	0		0	178 Anthracene
13	0	0	0	0	0		0	202 Fluoranthene
14	100	96	98	-2	260480	bb	1335	240 Chrysene-d12
15	100	90	97	2	423670	bb	1192	244 Terphenyl-d14
16	0	0	0	0	0		0	202 Pyrene
17	0	0	0	0	0		0	228 Benzo(a)anthracene
18	0	0	0	0	0		0	228 Chrysene
19	100	95	97	1	356020	bb	1554	264 Perylene-d12
20	0	0	0	0	0		0	252 Benzo(b)fluoranthene
21	0	0	0	0	0		0	252 Benzo(k)fluoranthene
22	0	0	0	0	0		0	252 Benzo(e)pyrene
23	0	0	0	0	0		0	252 Benzo(a)pyrene
24	0	0	0	0	0		0	252 Perylene
25	0	0	0	0	0		0	276 Indeno(1,2,3-cd)pyrene
26	0	0	0	0	0		0	278 Dibenz(a,h)anthracene
27	0	0	0	0	0		0	276 Benzo(g,h,i)perylene
28	0	0	0	0	0		0	266 Pentachlorophenol
29	100	94	97	1	185640	bb	382	82 Nitrobenzene-d5
30	100	97	99	0	339760	bb	644	172 2-Fluorobiphenyl
31	84	63	71	0	24976	bb	846	330 2,4,6-Tribromophenol
32	100	92	97	-1	171790	bb	272	99 Phenol-d5
33	100	90	98	2	461400	bb	1148	212 Pyrene-d10
34	100	93	99	0	493200	vb	953	188 Anthracene-d10
35	100	93	96	-1	67072	bb	487	240 1,4-Dibromobenzene-d4
36	98	82	86	1	113660	bb	429	185 1,3,5-Trichlorobenzene-d3

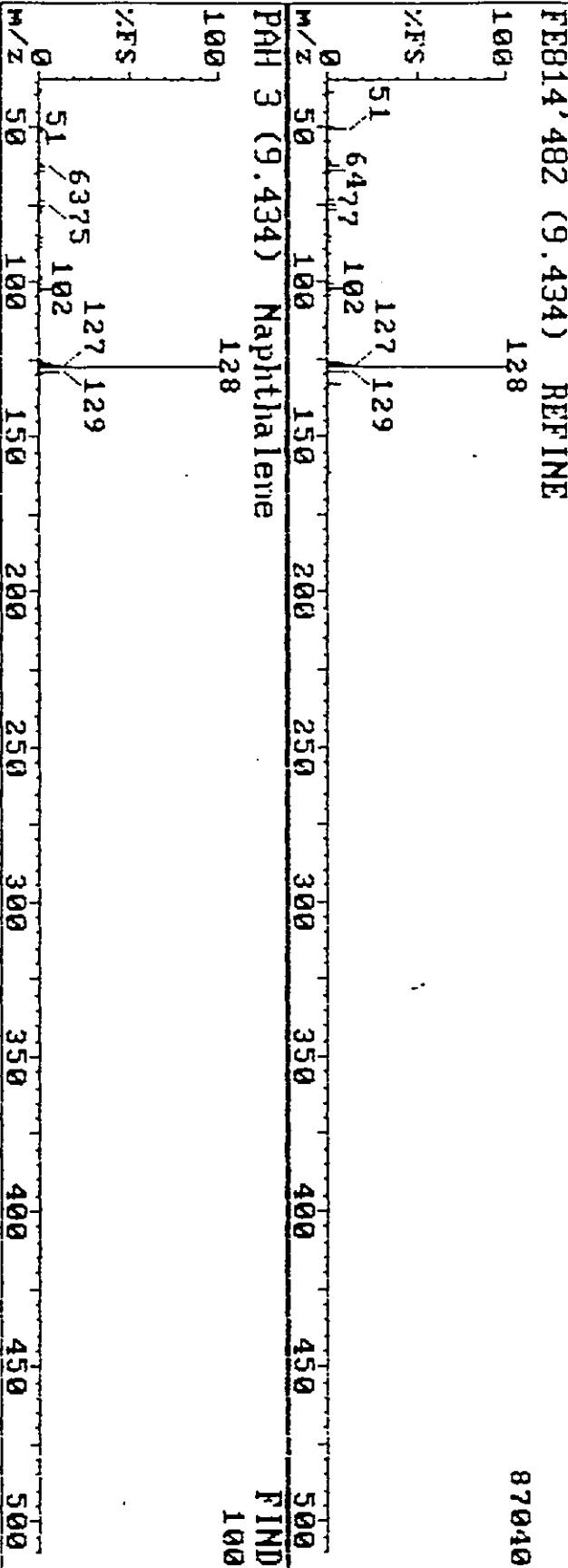
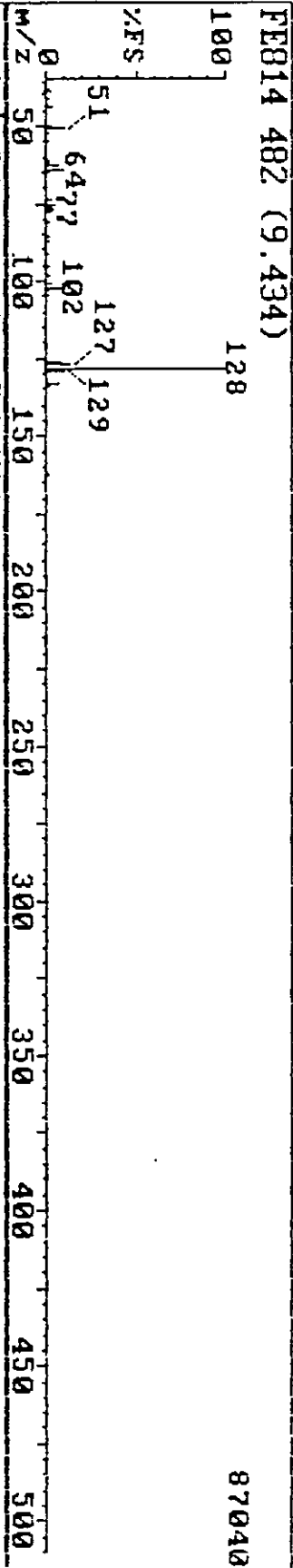
19-Sep-91 17:48

Sample: SBLK 091291 18976

Triangle Labs, Inc.

(919) 544-5729
Instrument F

2nd



VI. LABORATORY ANALYSIS

B. FORMALDEHYDE



**AMERICAN INTERPLEX
CORPORATION
LABORATORIES**

8600 Kanis Road
Little Rock, Arkansas 72204-2322
(501) 224-5060

Ramcon Environmental Corporation (C-488)
223 Scott Street
Memphis, TN 38112

October 14, 1991

ATTN: Mr. Joe Sewell

Control No. 4495

Description of Sample: Nine (9) impinger solution samples received on 10/3/91
Re: Lehman Roberts

Results:

<u>Sample Identification</u>	<u>Formaldehyde, mg</u>
D.I. Water Blank	<0.01
DNPH Blank	0.015
MeCl ₂ Blank	<0.01
Run 1	9.5
Run 2	11
Run 3	0.94

Method: EPA 8315

SL/td

AMERICAN INTERPLEX CORPORATION

By _____
Steven Lovell
Technical Director

VI. LABORATORY ANALYSIS

C. PARTICULATE

SAMPLE ANALYTICAL DATA FORM

Company Name LEHMAN ROBERTS-RM 202-FRONT HALF (ACETONE)

Sample Location _____ Relative Humidity in Lab 43 %

Blank Volume (V_a) 168 ml Density of Acetone (ρ_a) .7857 mg/ml

Date/Time wt. blank 9-6-91 11:30 AM Gross wt. 169.1139 g

Date/Time wt. blank 9-6-91 5:30 PM Gross wt. 169.1138 g

Ave. Gross wt. 169.1139 g

Tare wt. 169.1134 g

Weight of blank (m_{ab}) 0.0003 g

Acetone blank residue concentration (C_a): $(C_a) = (m_{ab}) / (V_a) (\rho_a) = (0.0000022 \text{ mg/g})$

Acetone Blank Wt.: $W_a = C_a V_{aw} \rho_a = (0.0000022) (291) (.7857) = (0.0005 \text{ g})$

	Run # 1	Run # 2	Run # 3
Acetone rinse volume (V_{aw}) ml	<u>291</u>	<u>291</u>	<u>291</u>
Date/Time of wt. <u>9-6-91 11:30 AM</u> Gross wt. g	<u>171.8832</u>	<u>171.7618</u>	<u>161.1763</u>
Date/Time of wt. <u>9-9-91 8:30 AM</u> Gross wt. g	<u>171.8827</u>	<u>171.7620</u>	<u>161.1761</u>
Average Gross wt. g	<u>171.8830</u>	<u>171.7619</u>	<u>161.1762</u>
Tare wt. g	<u>171.8718</u>	<u>171.7403</u>	<u>161.1538</u>
Less Acetone blank wt. (W_a) g	<u>0.0005</u>	<u>0.0005</u>	<u>0.0005</u>
Weight of particulate in acetone rinse (m_a) g	<u>0.0107</u>	<u>0.0211</u>	<u>0.0219</u>

Filter Numbers #	PT 5469	PT 5467	PT 5462
Date/Time of wt. <u>9-5-91 10 AM</u> Gross wt. g	<u>0.5652</u>	<u>0.5763</u>	<u>0.5725</u>
Date/Time of wt. <u>9-6-91 11:30 AM</u> Gross wt. g	<u>0.5657</u>	<u>0.5763</u>	<u>0.5724</u>
Average Gross wt. g	<u>0.5655</u>	<u>0.5763</u>	<u>0.5725</u>
Tare wt. g	<u>0.5614</u>	<u>0.5624</u>	<u>0.5624</u>

Weight of particulate on filter (m_f) g	<u>0.0041</u>	<u>0.0139</u>	<u>0.0101</u>
Weight of particulate in acetone rinse (m_a) g	<u>0.0107</u>	<u>0.0211</u>	<u>0.0219</u>
Total weight of particulate (m_n) g	<u>0.0148</u>	<u>0.0350</u>	<u>0.0320</u>

NOTE: In no case should a blank residue greater than 0.01 mg/g (or 0.001% of the blank weight) be subtracted from the sample weight.

Remarks: BROWN PARTICULATE PRESENT

Signature of Analyst [Signature] Signature of Reviewer _____

SAMPLE ANALYTICAL DATA FORM

Company Name LEHMAN-ROBERTS-RM202-BACKHALF (MeCl₂)

Sample Location _____ Relative Humidity in Lab 43 %

Blank Volume (V_a) 168 ml MeCl₂ BLANK Density of Acetone (ρ_a) 0.793255 mg/ml

Date/Time wt. blank _____ Gross wt. 134.1008 g

Date/Time wt. blank _____ Gross wt. 134.1006 g

Ave. Gross wt. 134.1007 g

Tare wt. 134.1011 g

Weight of blank (m_{ab}) 0.0004 g

MeCl₂ Acetone blank residue concentration (C_a): (C_a) = (m_{ab}) / (V_a) (ρ_a) = (0.0000016 mg/g)

MeCl₂ Acetone Blank Wt.: $W_a = C_a V_{aw} \rho_a = (0.0000016)(201)(1.3255) = (0.0004 \text{ g})$

	Run # 1	Run # 2	Run # 3
<u>MeCl₂</u> Acetone rinse volume (V _{aw}) ml	201	201	201
Date/Time of wt. <u>9-12-91 9:30 AM</u> Gross wt. g	125.4376	168.9698	175.5666
Date/Time of wt. <u>9-13-91 3:30 PM</u> Gross wt. g	125.4372	168.9695	175.5670
Average Gross wt. g	125.4374	168.9697	175.5668
Tare wt. g	125.4350	168.9670	175.5653
Less <u>MeCl₂</u> Acetone blank wt. (W _a) g	0.0004	0.0004	0.0004
Weight of particulate in acetone rinse (m _a) g	0.0020	0.0023	0.0011

Filter Numbers	#		
Date/Time of wt. _____	Gross wt. g		
Date/Time of wt. _____	Gross wt. g		
Average Gross wt. g			
Tare wt. g			

Weight of particulate on filter (m _f) g			
Weight of particulate in acetone rinse (m _a) g			
Total weight of particulate (m _n) g			

NOTE: In no case should a blank residue greater than 0.01 mg/g (or 0.001% of the blank weight) be subtracted from the sample weight.

Remarks: _____

Signature of Analyst [Signature] Signature of Reviewer _____

MINNESOTA BACK-HALF ANALYSIS

CHLOROFORM-ETHER EXTRACTION

Plant Location L. ROBERTS - RM202-CPM

Date 9-5-91

Sample Location _____

Relative Humidity in lab 43 %

Blank Volume (V_a) 150 ml

Di H₂O

Date/Time wt. blank 9-4-91 9 AM

Gross wt. 175.2107 g

Date/Time wt. blank 9-4-91 3 PM

Gross wt. 175.2145 g

Ave. Gross wt. 175.2116 g

Tare wt. 175.2104 g

Weight of blank Extract 0.0002 g

Impinger rinse volume _____ ml

Date/Time of wt 9-17-91 5 PM Gross wt g

Date/Time of wt 9-18-91 10 AM Gross wt g

Average Gross wt g

Tare wt g

Less Extract blank wt g

Wt of particulate in impinger rinse (m_a) g

Run # 1	Run # 2	Run # 3
1146	1269	1151
137.1410	164.5157	171.1155
137.1406	164.5152	171.1160
137.1408	164.5155	171.1160
137.1374	164.5155	171.1157
0.0002	0.0002	0.0002
0.0032	0.0073	0.0021

Remarks: _____

Signature of Analyst Sam Aug

Signature of Reviewer _____

RAMCON

ENVIRONMENTAL CORPORATION

AIR POLLUTION SOURCE TESTING AT

LEHMAN ROBERTS COMPANY
Memphis, Tennessee

VOLUME II

Submitted to:

LEHMAN ROBERT COMPANY
P.O. Box 666
Memphis, Tennessee 38101

and

NATIONAL ASPHALT PAVEMENT ASSOCIATION
5100 Forbes Boulevard
NAPA Building
Lanham, Maryland 20706-4413

Submitted on:

October 23, 1991

Submitted by:

RAMCON ENVIRONMENTAL CORPORATION
223 Scott Street
Memphis, Tennessee 38112
901/458-7000

VII. CALCULATIONS

A. PAH'S

SUMMARY OF TEST DATA

	9-3-91	9-3-91	9-3-91
	RUN #1	RUN #2	RUN #3

SAMPLING TRAIN DATA

		11:26	14:23	16:38
	start	11:26	14:23	16:38
	finish	12:38	15:30	17:44
1. Sampling time, minutes	Θ	60.0	60.0	60.0
2. Sampling nozzle diameter, in.	D_n	.2500	.2500	.2500
3. Sampling nozzle cross-sect. area, ft ²	A_n	.000341	.000341	.000341
4. Isokinetic variation	I	111.9	97.6	97.8
5. Sample gas volume - meter cond., cf.	V_m	37.776	38.113	39.703
6. Average meter temperature, °R	T_m	561	577	578
7. Avg. oriface pressure drop, in. H ₂ O	dH	1.34	1.32	1.39
8. Total PAH collected, mg.	M_n	0.6129	0.5402	0.6276

VELOCITY TRAVERSE DATA

9. Stack area, ft ²	A	13.80	13.80	13.80
10. Absolute stack gas pressure, in. Hg.	P_s	30.01	30.01	30.01
11. Barometric pressure, in. Hg.	P_{bar}	30.01	30.01	30.01
12. Avg. absolute stack temperature, R°	T_s	715	715	715
13. Average $\sqrt{\frac{2}{\rho} \Delta P}$, (C _p = .84)	$\sqrt{\frac{2}{\rho} \Delta P}$	0.89	0.95	0.98
14. Average stack gas velocity, ft./sec.	V_s	63.38	67.29	69.31

STACK MOISTURE CONTENT

15. Total water collected by train, ml.	V_{ic}	632.00	545.00	557.00
16. Moisture in stack gas, %	B_{ws}	46.21	43.03	42.63

EMISSIONS DATA

17. Stack gas flow rate, dscf/hr. (000's)	Q_{sd}	1254	1410	1463
18. Stack gas flow rate, cfm	acfm	52479	55716	57389
19. PAH concentration, gr/dscf	C_s	0.000272	0.000245	0.000273
20. PAH concentration, lb/hr	E	0.049	0.049	0.057
21.				

ORSAT DATA

22. Percent CO ₂ by volume	CO ₂	8.70	7.30	7.70
23. Percent O ₂ by volume	O ₂	4.70	5.70	5.00
24. Percent CO by volume	CO	.00	.00	.00
25. Percent N ₂ by volume	N ₂	86.60	87.00	87.30

$$V_{m(std)} = V_m \left[\frac{T_{(std)}}{T_m} \right] \left[\frac{P_{bar} + \frac{dH}{13.6}}{P_{(std)}} \right] = 17.64 \frac{^{\circ}R}{in.Hg} Y V_m \left[\frac{P_{bar} + \frac{dH}{13.6}}{T_m} \right]$$

Where:

- $V_{m(std)}$ = Dry Gas Volume through meter at standard conditions, cu. ft.
- V_m = Dry Gas Volume measured by meter, cu. ft.
- P_{bar} = Barometric pressure at oriface meter, in. Hg.
- P_{std} = Standard absolute pressure, (29.92 in. Hg.).
- T_m = Absolute temperature at meter $^{\circ}R$.
- T_{std} = Standard absolute temperature (528 $^{\circ}R$).
- dH = Average pressure drop across oriface meter, in. H₂O.
- Y = Dry gas meter calibration factor.
- 13.6 = Inches water per inches Hg.

RUN 1:

$$V_{m(std)} = (17.64)(.970)(37.776) \left[\frac{(30.01) + \frac{1.34}{13.6}}{561} \right] = 34.691 \text{ dscf}$$

RUN 2:

$$V_{m(std)} = (17.64)(.970)(38.113) \left[\frac{(30.01) + \frac{1.32}{13.6}}{577} \right] = 34.028 \text{ dscf}$$

RUN 3:

$$V_{m(std)} = (17.64)(.970)(39.703) \left[\frac{(30.01) + \frac{1.39}{13.6}}{578} \right] = 35.392 \text{ dscf}$$

Total Contaminants by Weight: GRAIN LOADING

concentration C'_s gr./dscf.

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

C'_s = Concentration of PAH in stack gas, dry basis, corrected to standard conditions, gr./dscf.

M_n = Total amount of PAH collected, mg.

$V_{m(\text{std})}$ = Dry gas volume through meter at standard conditions, cu. ft.

Run 1:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{0.6129}{34.691} \right] = 0.000272 \text{ gr./dscf.}$$

Run 2:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{0.5402}{34.028} \right] = 0.000245 \text{ gr./dscf.}$$

Run 3:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{0.6276}{35.392} \right] = 0.000273 \text{ gr./dscf.}$$

$$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + \%N_2)$$

Where:

M_d = Dry molecular weight, lb./lb.-mole.

$\%CO_2$ = Percent carbon dioxide by volume (dry basis).

$\%O_2$ = Percent oxygen by volume (dry basis).

$\%N_2$ = Percent nitrogen by volume (dry basis).

$\%CO$ = Percent carbon monoxide by volume (dry basis).

0.264 = Ratio of O_2 to N_2 in air, v/v.

0.28 = Molecular weight of N_2 or CO, divided by 100.

0.32 = Molecular weight of O_2 divided by 100.

0.44 = Molecular weight of CO_2 divided by 100.

Run 1:

$$M_d = 0.44(8.70\%) + 0.32(4.70\%) + 0.28(.00\% + 86.60\%) = 29.58 \frac{lb}{lb-mole}$$

Run 2:

$$M_d = 0.44(7.30\%) + 0.32(5.70\%) + 0.28(.00\% + 87.00\%) = 29.40 \frac{lb}{lb-mole}$$

Run 3:

$$M_d = 0.44(7.70\%) + 0.32(5.00\%) + 0.28(.00\% + 87.30\%) = 29.43 \frac{lb}{lb-mole}$$

$$V_{wc_{std}} = \left[V_f - V_i \right] \left[\frac{p_w R T_{(std)}}{M_w P_{(std)}} \right] = 0.04707 \left[V_f - V_i \right]$$

$$V_{wsg_{std}} = \left[W_f - W_i \right] \left[\frac{R T_{(std)}}{M_w P_{(std)}} \right] = 0.04715 \left[W_f - W_i \right]$$

Where:

0.04707 = Conversion factor, ft.³/ml.

0.04715 = Conversion factor, ft.³/g.

$V_{wc_{std}}$ = Volume of water vapor condensed (standard conditions), scf.

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel (standard conditions), ml.

$V_f - V_i$ = Final volume of impinger contents less initial volume, ml.

$W_f - W_i$ = Final weight of silica gel less initial weight, g.

p_w = Density of water, 0.002201 lb/ml.

R = Ideal gas constant, 21.85 in.Hg. (cu.ft./lb.-mole)(^oR).

M_w = Molecular weight of water vapor, 18.0 lb/lb-mole.

T_{std} = Absolute temperature at standard conditions, 528^oR.

P_{std} = Absolute pressure at standard conditions, 29.92 inches Hg.

Run 1:

$$V_{wc(std)} = (0.04707) (594.0) = 28.0 \text{ cu.ft}$$

$$V_{wsg(std)} = (0.04715) (38.0) = 1.8 \text{ cu.ft}$$

Run 2:

$$V_{wc(std)} = (0.04707) (516.0) = 24.3 \text{ cu.ft}$$

$$V_{wsg(std)} = (0.04715) (29.0) = 1.4 \text{ cu.ft}$$

Run 3:

$$V_{wc(std)} = (0.04707) (522.0) = 24.6 \text{ cu.ft}$$

$$V_{wsg(std)} = (0.04715) (35.0) = 1.7 \text{ cu.ft}$$

$$B_{ws} = \frac{V_{wc_{std}} + V_{wsg_{std}}}{V_{wc_{std}} + V_{wsg_{std}} + V_{m_{std}}} \times 100$$

Where:

B_{ws} = Proportion of water vapor, by volume, in the gas stream.

V_m = Dry gas volume measured by dry gas meter, (dcf).

$V_{wc_{std}}$ = Volume of water vapor condensed corrected to standard conditions (scf).

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel corrected to standard conditions (scf).

Run 1:

$$B_{ws} = \frac{28.0 + 1.8}{28.0 + 1.8 + 34.691} \times 100 = 46.21 \%$$

Run 2:

$$B_{ws} = \frac{24.3 + 1.4}{24.3 + 1.4 + 34.028} \times 100 = 43.03 \%$$

Run 3:

$$B_{ws} = \frac{24.6 + 1.7}{24.6 + 1.7 + 35.392} \times 100 = 42.63 \%$$

$$M_s = M_d (1 - B_{ws}) + 18 (B_{ws})$$

Where:

M_s = Molecular weight of stack gas, wet basis, (lb./lb.-mole).

M_d = Molecular weight of stack gas, dry basis, (lb./lb.-mole).

Run 1:

$$M_s = 29.58 (1 - 46.21) + 18 (46.21) = 24.23 (\text{lb./lb.-mole})$$

Run 2:

$$M_s = 29.40 (1 - 43.03) + 18 (43.03) = 24.49 (\text{lb./lb.-mole})$$

Run 3:

$$M_s = 29.43 (1 - 42.63) + 18 (42.63) = 24.56 (\text{lb./lb.-mole})$$

$$V_s = K_p C_p \left[\sqrt{dP} \right]_{\text{avg.}} \sqrt{\frac{T_s(\text{avg.})}{P_s M_s}}$$

Where:

- V_s = Average velocity of gas stream in stack, ft./sec.
- K_p = 85.49 ft/sec $\left[\frac{(\text{g/g-mole}) - (\text{mm Hg})}{(^{\circ}\text{K})(\text{mm H}_2\text{O})} \right]^{1/2}$
- C_p = Pitot tube coefficient, (dimensionless).
- dP = Velocity head of stack gas, in. H_2O .
- P_{bar} = Barometric pressure at measurement site, (in. Hg).
- P_g = Stack static pressure, (in. Hg).
- P_s = Absolute stack gas pressure, (in. Hg) = $P_{\text{bar}} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in. Hg).
- t_s = Stack temperature, ($^{\circ}\text{f}$).
- T_s = Absolute stack temperature, ($^{\circ}\text{R}$). = $460 + t_s$.
- M_s = Molecular weight of stack gas, wet basis, (lb/lb-mole).

Run 1:

$$V = (85.49) (.84) (0.89) \sqrt{\frac{715}{(30.01)(24.23)}} = 63.38 \text{ ft/sec.}$$

Run 2:

$$V = (85.49) (.84) (0.95) \sqrt{\frac{715}{(30.01)(24.49)}} = 67.29 \text{ ft/sec.}$$

Run 3:

$$V = (85.49) (.84) (0.98) \sqrt{\frac{715}{(30.01)(24.56)}} = 69.31 \text{ ft/sec.}$$

$$Q_{sd} = 3600 \left[1 - B_{wc} \right] V_s A \left[\frac{T_{std}}{T_{stk}} \right] \left[\frac{P_s}{P_{std}} \right]$$

Where:

- Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, (dscf/hr).
- A = Cross sectional area of stack, (ft.²).
- 3600 = Conversion factor, (sec./hr.).
- t_s = Stack temperature, (°f).
- T_s = Absolute stack temperature, (°R).
- T_{std} = Standard absolute temperature, (528°R).
- P_{bar} = Barometric pressure at measurement site, (in.Hg.).
- P_g = Stack static pressure, (in.Hg.).
- P_s = Absolute stack gas pressure, (in.Hg.); = $P_{bar} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in.Hg.).

Run 1:

$$Q_{sd} = 3600(1 - .4621)(63.38)(13.80) \left[\frac{528}{715} \right] \left[\frac{30.01}{29.92} \right] = 1,254,491.3 \frac{\text{dscf}}{\text{hr}}$$

Run 2:

$$Q_{sd} = 3600(1 - .4303)(67.29)(13.80) \left[\frac{528}{715} \right] \left[\frac{30.01}{29.92} \right] = 1,410,621.9 \frac{\text{dscf}}{\text{hr}}$$

Run 3:

$$Q_{sd} = 3600(1 - .4263)(69.31)(13.80) \left[\frac{528}{715} \right] \left[\frac{30.01}{29.92} \right] = 1,463,169.4 \frac{\text{dscf}}{\text{hr}}$$

Emissions Rate from Stack

$$E = \frac{(C_s) (Q_{sd})}{7000 \text{ gr./lb.}} = \text{lb. / hr.}$$

Where:

E = Emissions rate, lb/hr.

C_s = Concentration of PAH in stack gas, dry basis, corrected to standard conditions, gr/dscf.

Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run 1:

$$E = \frac{(0.000272) (1254491.3)}{7000} = 0.049 \text{ lb. / hr.}$$

Run 2:

$$E = \frac{(0.000245) (1410621.9)}{7000} = 0.049 \text{ lb. / hr.}$$

Run 3:

$$E = \frac{(0.000273) (1463169.4)}{7000} = 0.057 \text{ lb. / hr.}$$

$$I = 100 T_s \left[\frac{0.002669 V_{ic} + \frac{(V_m / T_m) (P_{bar} + dH / 13.6)}{60 \theta V_s P_s A_n} \right]$$

Where:

- I = Percent isokinetic sampling.
- 100 = Conversion to percent.
- T_s = Absolute average stack gas temperature, °R.
- 0.002669 = Conversion factor, Hg - ft³/ml - °R.
- V_{ic} = Ttl vol of liquid collected in impingers and silica gel, ml.
- T_m = Absolute average dry gas meter temperature, °R.
- P_{bar} = Barometric pressure at sampling site, (in. Hg).
- dH = Av pressure differential across the oriface meter, (in.H₂O).
- 13.6 = Specific gravity of mercury.
- 60 = Conversion seconds to minutes.
- θ = Total sampling time, minutes.
- V_s = Stack gas velocity, ft./sec.
- P_s = Absolute stack gas pressure, in. Hg.
- A_n = Cross sectional area of nozzle, ft².

Run 1:

$$I = (100)(715) \left[\frac{(0.002669)(632.0) + \frac{37.776}{561} \left[30.01 + \frac{1.34}{13.6} \right]}{60 (60.0) (63.38) (30.01) (.000341)} \right] = 111.9\%$$

Run 2:

$$I = (100)(715) \left[\frac{(0.002669)(545.0) + \frac{38.113}{577} \left[30.01 + \frac{1.32}{13.6} \right]}{60 (60.0) (67.29) (30.01) (.000341)} \right] = 97.6\%$$

Run 3:

$$I = (100)(715) \left[\frac{(0.002669)(557.0) + \frac{39.703}{578} \left[30.01 + \frac{1.39}{13.6} \right]}{60 (60.0) (69.31) (30.01) (.000341)} \right] = 97.8\%$$

$$\% E_a = \frac{100 \times (\% O_2) - 0.5 (\% CO)}{0.264 (\% N_2) - (\% O_2) + 0.5 (\% CO)}$$

- Where: %E_a = Percent excess air.
%O₂ = Percent oxygen by volume, dry basis.
%CO = Percent carbon monoxide by volume, dry basis.
%CO₂ = Percent carbon dioxide by volume, dry basis.
%N₂ = Percent nitrogen by volume, dry basis.

Run # 1: $\frac{100 \times (\% 4.70) - .05 (\% .00)}{0.264 (\% 86.60) - (\% 4.70) + 0.5 (\% .00)} = 25.9 \%$

Run # 2: $\frac{100 \times (\% 5.70) - .05 (\% .00)}{0.264 (\% 87.00) - (\% 5.70) + 0.5 (\% .00)} = 33.0 \%$

Run # 3: $\frac{100 \times (\% 5.00) - .05 (\% .00)}{0.264 (\% 87.30) - (\% 5.00) + 0.5 (\% .00)} = 27.7 \%$

VII. CALCULATIONS

B. FORMALDEHYDE

SUMMARY OF TEST DATA

	9-30-91	9-30-91	9-30-91
	RUN #1	RUN #2	RUN #3

SAMPLING TRAIN DATA

		10:56	13:42	16:13
	start	10:56	13:42	16:13
	finish	12:24	14:59	17:30
1. Sampling time, minutes	Θ	72.0	72.0	72.0
2. Sampling nozzle diameter, in.	D_n	.2700	.2700	.2700
3. Sampling nozzle cross-sect. area, ft ²	A_n	.000398	.000398	.000398
4. Isokinetic variation	I	98.5	99.5	98.6
5. Sample gas volume - meter cond., cf.	V_m	51.918	52.036	52.728
6. Average meter temperature, °R	T_m	553	561	565
7. Avg. oriface pressure drop, in. H ₂ O	dH	1.31	1.28	1.30
8. Total formaldehyde collected, mg.	M_n	9.50	11.00	.94

VELOCITY TRAVERSE DATA

9. Stack area, ft ²	A	13.88	13.88	13.88
10. Absolute stack gas pressure, in. Hg.	P_s	30.15	30.15	30.15
11. Barometric pressure, in. Hg.	P_{bar}	30.15	30.15	30.15
12. Avg. absolute stack temperature, R°	T_s	697	707	701
13. Average $-\sqrt{v_{el. head}}$, ($C_p = .84$)	$-\sqrt{dP}$	0.81	0.81	0.81
14. Average stack gas velocity, ft./sec.	V_s	55.02	55.37	55.19

STACK MOISTURE CONTENT

15. Total water collected by train, ml.	V_{ic}	434.60	450.50	437.90
16. Moisture in stack gas, %	B_{ws}	28.82	29.76	29.04

EMISSIONS DATA

17. Stack gas flow rate, dscf/hr.(000's)	Q_{sd}	1493	1462	1485
18. Stack gas flow rate, cfm	acfm	45821	46112	45962
19. Formaldehyde concentration, gr/dscf	C_s	0.0029	0.0034	0.0003
20. Formaldehyde concentration, lb/hr	E	0.62	0.71	0.06
21. concentration, lb/mBtu	E'	0.00000	0.00000	0.00000

ORSAT DATA

22. Percent CO ₂ by volume	CO ₂	2.00	4.30	2.20
23. Percent O ₂ by volume	O ₂	17.40	13.30	17.10
24. Percent CO by volume	CO	.00	.00	.00
25. Percent N ₂ by volume	N ₂	80.60	82.40	80.70

$$V_{m(std)} = V_m \left[\frac{T_{(std)}}{T_m} \right] \left[\frac{P_{bar} + \frac{dH}{13.6}}{P_{(std)}} \right] = 17.64 \frac{^{\circ}R}{in.Hg} Y V_m \left[\frac{P_{bar} + \frac{dH}{13.6}}{T_m} \right]$$

Where:

$V_{m(std)}$ = Dry Gas Volume through meter at standard conditions, cu. ft.

V_m = Dry Gas Volume measured by meter, cu. ft.

P_{bar} = Barometric pressure at oriface meter, in. Hg.

P_{std} = Standard absolute pressure, (29.92 in. Hg.).

T_m = Absolute temperature at meter $^{\circ}R$.

T_{std} = Standard absolute temperature (528 $^{\circ}R$).

dH = Average pressure drop across oriface meter, in. H₂O.

Y = Dry gas meter calibration factor.

13.6 = Inches water per inches Hg.

RUN 1:

$$V_{m(std)} = (17.64)(1.011)(51.918) \left[\frac{(30.15) + \frac{1.31}{13.6}}{553} \right] = 50.643 \text{ dscf}$$

RUN 2:

$$V_{m(std)} = (17.64)(1.011)(52.036) \left[\frac{(30.15) + \frac{1.28}{13.6}}{561} \right] = 50.030 \text{ dscf}$$

RUN 3:

$$V_{m(std)} = (17.64)(1.011)(52.728) \left[\frac{(30.15) + \frac{1.30}{13.6}}{565} \right] = 50.339 \text{ dscf}$$

Total Contaminants by Weight: GRAIN LOADING

concentration C'_s gr./dscf.

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

C'_s = Concentration of formaldehyde in stack gas, dry basis, corrected to standard conditions, gr./dscf.

M_n = Total amount of formaldehyde collected, mg.

$V_{m(\text{std})}$ = Dry gas volume through meter at standard conditions, cu. ft.

Run 1:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{9.50}{50.643} \right] = 0.0029 \text{ gr./dscf.}$$

Run 2:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{11.00}{50.030} \right] = 0.0034 \text{ gr./dscf.}$$

Run 3:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{.94}{50.339} \right] = 0.0003 \text{ gr./dscf.}$$

$$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + \%N_2)$$

Where:

M_d = Dry molecular weight, lb./lb.-mole.

$\%CO_2$ = Percent carbon dioxide by volume (dry basis).

$\%O_2$ = Percent oxygen by volume (dry basis).

$\%N_2$ = Percent nitrogen by volume (dry basis).

$\%CO$ = Percent carbon monoxide by volume (dry basis).

0.264 = Ratio of O_2 to N_2 in air, v/v.

0.28 = Molecular weight of N_2 or CO, divided by 100.

0.32 = Molecular weight of O_2 divided by 100.

0.44 = Molecular weight of CO_2 divided by 100.

Run 1:

$$M_d = 0.44(2.00\%) + 0.32(17.40\%) + 0.28(.00\% + 80.60\%) = 29.02 \frac{lb}{lb-mole}$$

Run 2:

$$M_d = 0.44(4.30\%) + 0.32(13.30\%) + 0.28(.00\% + 82.40\%) = 29.22 \frac{lb}{lb-mole}$$

Run 3:

$$M_d = 0.44(2.20\%) + 0.32(17.10\%) + 0.28(.00\% + 80.70\%) = 29.04 \frac{lb}{lb-mole}$$

$$V_{wc_{std}} = \left[V_f - V_i \right] \left[\frac{P_w R T_{(std)}}{M_w P_{(std)}} \right] = 0.04707 \left[V_f - V_i \right]$$

$$V_{wsg_{std}} = \left[W_f - W_i \right] \left[\frac{R T_{(std)}}{M_w P_{(std)}} \right] = 0.04715 \left[W_f - W_i \right]$$

Where:

0.04707 = Conversion factor, ft.³/ml.

0.04715 = Conversion factor, ft.³/g.

$V_{wc_{std}}$ = Volume of water vapor condensed (standard conditions), scf.

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel (standard conditions), ml.

$V_f - V_i$ = Final volume of impinger contents less initial volume, ml.

$W_f - W_i$ = Final weight of silica gel less initial weight, g.

P_w = Density of water, 0.002201 lb/ml.

R = Ideal gas constant, 21.85 in.Hg. (cu.ft./lb.-mole)(^oR).

M_w = Molecular weight of water vapor, 18.0 lb/lb-mole.

T_{std} = Absolute temperature at standard conditions, 528^oR.

P_{std} = Absolute pressure at standard conditions, 29.92 inches Hg.

Run 1:

$$\begin{aligned} V_{wc(std)} &= (0.04707) (416.0) = 19.6 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) (18.6) = 0.9 \text{ cu.ft} \end{aligned}$$

Run 2:

$$\begin{aligned} V_{wc(std)} &= (0.04707) (430.0) = 20.2 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) (20.5) = 1.0 \text{ cu.ft} \end{aligned}$$

Run 3:

$$\begin{aligned} V_{wc(std)} &= (0.04707) (420.0) = 19.8 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) (17.9) = 0.8 \text{ cu.ft} \end{aligned}$$

Moisture Content of Stack Gases

$$B_{ws} = \frac{V_{wc_{std}} + V_{wsg_{std}}}{V_{wc_{std}} + V_{wsg_{std}} + V_{m_{std}}} \times 100$$

Where:

B_{ws} = Proportion of water vapor, by volume, in the gas stream.

V_m = Dry gas volume measured by dry gas meter, (dcf).

$V_{wc_{std}}$ = Volume of water vapor condensed corrected to standard conditions (scf).

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel corrected to standard conditions (scf).

Run 1:

$$B_{ws} = \frac{19.6 + 0.9}{19.6 + 0.9 + 50.643} \times 100 = 28.82 \%$$

Run 2:

$$B_{ws} = \frac{20.2 + 1.0}{20.2 + 1.0 + 50.030} \times 100 = 29.76 \%$$

Run 3:

$$B_{ws} = \frac{19.8 + 0.8}{19.8 + 0.8 + 50.339} \times 100 = 29.04 \%$$

$$B_{ws} = \frac{V_{wc_{std}} + V_{wsg_{std}}}{V_{wc_{std}} + V_{wsg_{std}} + V_{m_{std}}} \times 100$$

Where:

B_{ws} = Proportion of water vapor, by volume, in the gas stream.

V_m = Dry gas volume measured by dry gas meter, (dcf).

$V_{wc_{std}}$ = Volume of water vapor condensed corrected to standard conditions (scf).

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel corrected to standard conditions (scf).

Run 1:

$$B_{ws} = \frac{19.6 + 0.9}{19.6 + 0.9 + 50.643} \times 100 = 28.82 \%$$

Run 2:

$$B_{ws} = \frac{20.2 + 1.0}{20.2 + 1.0 + 50.030} \times 100 = 29.76 \%$$

Run 3:

$$B_{ws} = \frac{19.8 + 0.8}{19.8 + 0.8 + 50.339} \times 100 = 29.04 \%$$

$$M_s = M_d (1 - B_{ws}) + 18 (B_{ws})$$

Where:

M_s = Molecular weight of stack gas, wet basis, (lb./lb.-mole).

M_d = Molecular weight of stack gas, dry basis, (lb./lb.-mole).

Run 1:

$$M_s = 29.02 (1 - 28.82) + 18 (28.82) = 25.84 (\text{lb./lb.-mole})$$

Run 2:

$$M_s = 29.22 (1 - 29.76) + 18 (29.76) = 25.88 (\text{lb./lb.-mole})$$

Run 3:

$$M_s = 29.04 (1 - 29.04) + 18 (29.04) = 25.83 (\text{lb./lb.-mole})$$

$$V_s = K_p C_p \left[\sqrt{dP} \right] \text{ avg. } \sqrt{\frac{T_s(\text{avg.})}{P_s M_s}}$$

Where:

- V_s = Average velocity of gas stream in stack, ft./sec.
- K_p = 85.49 ft/sec $\left[\frac{(\text{g/g-mole}) - (\text{mm Hg})}{(^{\circ}\text{K}) (\text{mm H}_2\text{O})} \right]^{1/2}$
- C_p = Pitot tube coefficient, (dimensionless).
- dP = Velocity head of stack gas, in. H_2O .
- P_{bar} = Barometric pressure at measurement site, (in. Hg).
- P_g = Stack static pressure, (in. Hg).
- P_s = Absolute stack gas pressure, (in. Hg) = $P_{\text{bar}} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in. Hg).
- t_s = Stack temperature, ($^{\circ}\text{f}$).
- T_s = Absolute stack temperature, ($^{\circ}\text{R}$). = 460 + t_s .
- M_s = Molecular weight of stack gas, wet basis, (lb/lb-mole).

Run 1:

$$V = (85.49) (.84) (0.81) \sqrt{\frac{697}{(30.15)(25.84)}} = 55.02 \text{ ft/sec.}$$

Run 2:

$$V = (85.49) (.84) (0.81) \sqrt{\frac{707}{(30.15)(25.88)}} = 55.37 \text{ ft/sec.}$$

Run 3:

$$V = (85.49) (.84) (0.81) \sqrt{\frac{701}{(30.15)(25.83)}} = 55.19 \text{ ft/sec.}$$

$$Q_{sd} = 3600 \left[1 - B_{wc} \right] V_s A \left[\frac{T_{std}}{T_{stk}} \right] \left[\frac{P_s}{P_{std}} \right]$$

Where:

- Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, (dscf/hr).
- A = Cross sectional area of stack, (ft.²).
- 3600 = Conversion factor, (sec./hr.).
- t_s = Stack temperature, (°f).
- T_s = Absolute stack temperature, (°R).
- T_{std} = Standard absolute temperature, (528°R).
- P_{bar} = Barometric pressure at measurement site, (in.Hg.).
- P_g = Stack static pressure, (in.Hg.).
- P_s = Absolute stack gas pressure, (in.Hg.); = $P_{bar} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in.Hg.).

Run 1:

$$Q_{sd} = 3600(1 - .2882)(55.02)(13.88) \left[\frac{528}{697} \right] \left[\frac{30.15}{29.92} \right] = 1493817.0 \frac{\text{dscf}}{\text{hr}}$$

Run 2:

$$Q_{sd} = 3600(1 - .2976)(55.37)(13.88) \left[\frac{528}{707} \right] \left[\frac{30.15}{29.92} \right] = 1462484.4 \frac{\text{dscf}}{\text{hr}}$$

Run 3:

$$Q_{sd} = 3600(1 - .2904)(55.19)(13.88) \left[\frac{528}{701} \right] \left[\frac{30.15}{29.92} \right] = 1485277.5 \frac{\text{dscf}}{\text{hr}}$$

$$E = \frac{(C_s) (Q_{sd})}{7000 \text{ gr./lb.}} = \text{lb. / hr.}$$

Where:

E = Emissions rate, lb/hr.

C_s = Concentration of formaldehyde in stack gas, dry basis, corrected to standard conditions, gr/dscf.

Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run 1:

$$E = \frac{(0.0029) (1493817.0)}{7000} = 0.62 \text{ lb. / hr.}$$

Run 2:

$$E = \frac{(0.0034) (1462484.4)}{7000} = 0.71 \text{ lb. / hr.}$$

Run 3:

$$E = \frac{(0.0003) (1485277.5)}{7000} = 0.06 \text{ lb. / hr.}$$

$$I = 100 T_s \left[\frac{0.002669 V_{ic} + \frac{(V_m / T_m) (P_{bar} + dH / 13.6)}{60 \theta V_s P_s A_n} \right]$$

Where:

- I = Percent isokinetic sampling.
- 100 = Conversion to percent.
- T_s = Absolute average stack gas temperature, °R.
- 0.002669 = Conversion factor, Hg - ft³/ml - °R.
- V_{ic} = Ttl vol of liquid collected in impingers and silica gel, ml.
- T_m = Absolute average dry gas meter temperature, °R.
- P_{bar} = Barometric pressure at sampling site, (in. Hg).
- dH = Av pressure differential across the oriface meter, (in.H₂O).
- 13.6 = Specific gravity of mercury.
- 60 = Conversion seconds to minutes.
- θ = Total sampling time, minutes.
- V_s = Stack gas velocity, ft./sec.
- P_s = Absolute stack gas pressure, in. Hg.
- A_n = Cross sectional area of nozzle, ft².

Run 1:

$$I = (100)(697) \left[\frac{(0.002669)(434.6) + \frac{51.918}{553} \left[30.15 + \frac{1.31}{13.6} \right]}{60 (72.0) (55.02) (30.15) (.000398)} \right] = 98.5\%$$

Run 2:

$$I = (100)(707) \left[\frac{(0.002669)(450.5) + \frac{52.036}{561} \left[30.15 + \frac{1.28}{13.6} \right]}{60 (72.0) (55.37) (30.15) (.000398)} \right] = 99.5\%$$

Run 3:

$$I = (100)(701) \left[\frac{(0.002669)(437.9) + \frac{52.728}{565} \left[30.15 + \frac{1.30}{13.6} \right]}{60 (72.0) (55.19) (30.15) (.000398)} \right] = 98.6\%$$

$$\% E_a = \frac{100 \times (\% O_2) - 0.5 (\% CO)}{0.264 (\% N_2) - (\% O_2) + 0.5 (\% CO)}$$

- Where: %E_a = Percent excess air.
%O₂ = Percent oxygen by volume, dry basis.
%CO = Percent carbon monoxide by volume, dry basis.
%CO₂ = Percent carbon dioxide by volume, dry basis.
%N₂ = Percent nitrogen by volume, dry basis.

Run # 1:
$$\frac{100 \times (\% 17.40) - .05 (\% .00)}{0.264 (\% 80.60) - (\% 17.40) + 0.5 (\% .00)} = 448.6 \%$$

Run # 2:
$$\frac{100 \times (\% 13.30) - .05 (\% .00)}{0.264 (\% 82.40) - (\% 13.30) + 0.5 (\% .00)} = 157.3 \%$$

Run # 3:
$$\frac{100 \times (\% 17.10) - .05 (\% .00)}{0.264 (\% 80.70) - (\% 17.10) + 0.5 (\% .00)} = 406.7 \%$$

VII. CALCULATIONS

C. PARTICULATE & CONDENSIBLE PM

LEHMAN ROBERTS - FOR NAPA
 MPHS, TN PART. (PM) & CONDENSIBLE (CPM)

SUMMARY OF TEST DATA

9-4-91 9-4-91 9-4-91
 RUN #1 RUN #2 RUN #3

SAMPLING TRAIN DATA

		09:52	11:43	13:29
	start	09:52	11:43	13:29
	finish	10:57	12:48	14:34
1. Sampling time, minutes	Θ	60.0	60.0	60.0
2. Sampling nozzle diameter, in.	D_n	.2500	.2500	.2500
3. Sampling nozzle cross-sect. area, ft ²	A_n	.000341	.000341	.000341
4. Isokinetic variation	I	96.3	114.2	107.0
5. Sample gas volume - meter cond., cf.	V_m	37.235	41.834	41.393
6. Average meter temperature, °R	T_m	564	570	575
7. Avg. oriface pressure drop, in. H ₂ O	dH	1.29	1.58	1.51
8. Total particulate collected, mg.	M_n	14.80	35.00	32.00

VELOCITY TRAVERSE DATA

9. Stack area, ft ²	A	13.75	13.75	13.75
10. Absolute stack gas pressure, in. Hg.	P_s	30.06	30.06	30.06
11. Barometric pressure, in. Hg.	P_{bar}	30.06	30.06	30.06
12. Avg. absolute stack temperature, R°	T_s	720	740	740
13. Average $-\sqrt{vel. head}$, ($C_p = .84$)	$-\sqrt{dP}$	0.95	0.93	0.97
14. Average stack gas velocity, ft./sec.	V_s	66.90	67.03	70.50

STACK MOISTURE CONTENT

15. Total water collected by train, ml.	V_{ic}	514.00	625.00	620.00
16. Moisture in stack gas, %	B_{ws}	41.54	43.69	44.00

EMISSIONS DATA

17. Stack gas flow rate, dscf/hr. (000's)	Q_{sd}	1426	1339	1400
18. Stack gas flow rate, cfm	acfm	55193	55300	58163
19. Particulate concentration, gr/dscf	C_s	0.0067	0.0142	0.0133
20. Particulate concentration, lb/hr	E	1.37	2.72	2.66
21.				

ORSAT DATA

22. Percent CO ₂ by volume	CO ₂	9.20	7.70	4.00
23. Percent O ₂ by volume	O ₂	8.70	5.00	3.20
24. Percent CO by volume	CO	.00	.00	.00
25. Percent N ₂ by volume	N ₂	82.10	87.30	92.80

$$V_{m(std)} = V_m \left[\frac{T_{(std)}}{T_m} \right] \left[\frac{P_{bar} + \frac{dH}{13.6}}{P_{(std)}} \right] = 17.64 \frac{^{\circ}R}{in.Hg} Y V_m \left[\frac{P_{bar} + \frac{dH}{13.6}}{T_m} \right]$$

Where:

$V_{m(std)}$ = Dry Gas Volume through meter at standard conditions, cu. ft.

V_m = Dry Gas Volume measured by meter, cu. ft.

P_{bar} = Barometric pressure at oriface meter, in. Hg.

P_{std} = Standard absolute pressure, (29.92 in. Hg.).

T_m = Absolute temperature at meter $^{\circ}R$.

T_{std} = Standard absolute temperature (528 $^{\circ}R$).

dH = Average pressure drop across oriface meter, in. H₂O.

Y = Dry gas meter calibration factor.

13.6 = Inches water per inches Hg.

RUN 1:

$$V_{m(std)} = (17.64)(.970)(37.235) \left[\frac{(30.06) + \frac{1.29}{13.6}}{564} \right] = 34.064 \text{ dscf}$$

0.9647125

RUN 2:

$$V_{m(std)} = (17.64)(.970)(41.834) \left[\frac{(30.06) + \frac{1.58}{13.6}}{570} \right] = 37.896 \text{ dscf}$$

RUN 3:

$$V_{m(std)} = (17.64)(.970)(41.393) \left[\frac{(30.06) + \frac{1.51}{13.6}}{575} \right] = 37.164 \text{ dscf}$$

Particulate concentration C'_S gr./dscf.

$$C'_S = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

C'_S = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr./dscf.

M_n = Total amount of particulate matter collected, mg.

$V_{m(\text{std})}$ = Dry gas volume through meter at standard conditions, cu. ft.

Run 1:

$$C'_S = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{14.80}{34.064} \right] = 0.0067 \text{ gr./dscf.}$$

Run 2:

$$C'_S = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{35.00}{37.896} \right] = 0.0142 \text{ gr./dscf.}$$

Run 3:

$$C'_S = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{32.00}{37.164} \right] = 0.0133 \text{ gr./dscf.}$$

Total Contaminants by Weight: GRAIN LOADING
(CPM)

Particulate concentration C'_s gr./dscf.

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

C'_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr./dscf.

M_n = Total amount of particulate matter collected, mg.

$V_{m(\text{std})}$ = Dry gas volume through meter at standard conditions, cu. ft.

Run 1:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{5.20}{34.064} \right] = 0.0024 \text{ gr./dscf.}$$

Run 2:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{5.10}{37.896} \right] = 0.0021 \text{ gr./dscf.}$$

Run 3:

$$C'_s = \left[0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[\frac{3.20}{37.164} \right] = 0.0013 \text{ gr./dscf.}$$

$$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + \%N_2)$$

Where:

M_d = Dry molecular weight, lb./lb.-mole.

$\%CO_2$ = Percent carbon dioxide by volume (dry basis).

$\%O_2$ = Percent oxygen by volume (dry basis).

$\%N_2$ = Percent nitrogen by volume (dry basis).

$\%CO$ = Percent carbon monoxide by volume (dry basis).

0.264 = Ratio of O_2 to N_2 in air, v/v.

0.28 = Molecular weight of N_2 or CO, divided by 100.

0.32 = Molecular weight of O_2 divided by 100.

0.44 = Molecular weight of CO_2 divided by 100.

Run 1:

$$M_d = 0.44(9.20\%) + 0.32(8.70\%) + 0.28(.00\% + 82.10\%) = 29.82 \frac{lb}{lb-mole}$$

Run 2:

$$M_d = 0.44(7.70\%) + 0.32(5.00\%) + 0.28(.00\% + 87.30\%) = 29.43 \frac{lb}{lb-mole}$$

Run 3:

$$M_d = 0.44(4.00\%) + 0.32(3.20\%) + 0.28(.00\% + 92.80\%) = 28.77 \frac{lb}{lb-mole}$$

$$V_{wc_{std}} = \left[V_f - V_i \right] \left[\frac{P_w R T_{(std)}}{M_w P_{(std)}} \right] = 0.04707 \left[V_f - V_i \right]$$

$$V_{wsg_{std}} = \left[W_f - W_i \right] \left[\frac{R T_{(std)}}{M_w P_{(std)}} \right] = 0.04715 \left[W_f - W_i \right]$$

Where:

0.04707 = Conversion factor, ft.³/ml.

0.04715 = Conversion factor, ft.³/g.

$V_{wc_{std}}$ = Volume of water vapor condensed (standard conditions), scf.

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel (standard conditions), ml.

$V_f - V_i$ = Final volume of impinger contents less initial volume, ml.

$W_f - W_i$ = Final weight of silica gel less initial weight, g.

P_w = Density of water, 0.002201 lb/ml.

R = Ideal gas constant, 21.85 in.Hg. (cu.ft./lb.-mole)(^oR).

M_w = Molecular weight of water vapor, 18.0 lb/lb-mole.

T_{std} = Absolute temperature at standard conditions, 528^oR.

P_{std} = Absolute pressure at standard conditions, 29.92 inches Hg.

Run 1:

$$\begin{aligned} V_{wc(std)} &= (0.04707) (492.0) = 23.2 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) (22.0) = 1.0 \text{ cu.ft} \end{aligned}$$

Run 2:

$$\begin{aligned} V_{wc(std)} &= (0.04707) (595.0) = 28.0 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) (30.0) = 1.4 \text{ cu.ft} \end{aligned}$$

Run 3:

$$\begin{aligned} V_{wc(std)} &= (0.04707) (590.0) = 27.8 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) (30.0) = 1.4 \text{ cu.ft} \end{aligned}$$

$$B_{ws} = \frac{V_{wc_{std}} + V_{wsg_{std}}}{V_{wc_{std}} + V_{wsg_{std}} + V_{m_{std}}} \times 100$$

Where:

B_{ws} = Proportion of water vapor, by volume, in the gas stream.

V_m = Dry gas volume measured by dry gas meter, (dcf).

$V_{wc_{std}}$ = Volume of water vapor condensed corrected to standard conditions (scf).

$V_{wsg_{std}}$ = Volume of water vapor collected in silica gel corrected to standard conditions (scf).

Run 1:

$$B_{ws} = \frac{23.2 + 1.0}{23.2 + 1.0 + 34.064} \times 100 = 41.54 \%$$

Run 2:

$$B_{ws} = \frac{28.0 + 1.4}{28.0 + 1.4 + 37.896} \times 100 = 43.69 \%$$

Run 3:

$$B_{ws} = \frac{27.8 + 1.4}{27.8 + 1.4 + 37.164} \times 100 = 44.00 \%$$

$$M_s = M_d (1 - B_{ws}) + 18 (B_{ws})$$

Where:

M_s = Molecular weight of stack gas, wet basis, (lb./lb.-mole).

M_d = Molecular weight of stack gas, dry basis, (lb./lb.-mole).

Run 1:

$$M_s = 29.82 (1 - 41.54) + 18 (41.54) = 24.91 (lb./lb.-mole)$$

Run 2:

$$M_s = 29.43 (1 - 43.69) + 18 (43.69) = 24.44 (lb./lb.-mole)$$

Run 3:

$$M_s = 28.77 (1 - 44.00) + 18 (44.00) = 24.03 (lb./lb.-mole)$$

$$V_s = K_p C_p \left[\sqrt{dP} \right] \text{ avg. } \sqrt{\frac{T_s(\text{avg.})}{P_s M_s}}$$

Where:

- V_s = Average velocity of gas stream in stack, ft./sec.
- K_p = 85.49 ft/sec $\left[\frac{(\text{g/g-mole}) - (\text{mm Hg})}{(^{\circ}\text{K})(\text{mm H}_2\text{O})} \right]^{1/2}$
- C_p = Pitot tube coefficient, (dimensionless).
- dP = Velocity head of stack gas, in. H_2O .
- P_{bar} = Barometric pressure at measurement site, (in. Hg).
- P_g = Stack static pressure, (in. Hg).
- P_s = Absolute stack gas pressure, (in. Hg) = $P_{\text{bar}} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in. Hg).
- t_s = Stack temperature, ($^{\circ}\text{f}$).
- T_s = Absolute stack temperature, ($^{\circ}\text{R}$). = 460 + t_s .
- M_s = Molecular weight of stack gas, wet basis, (lb/lb-mole).

Run 1:

$$V = (85.49) (.84) (0.95) \sqrt{\frac{720}{(30.06)(24.91)}} = 66.90 \text{ ft/sec.}$$

Run 2:

$$V = (85.49) (.84) (0.93) \sqrt{\frac{740}{(30.06)(24.44)}} = 67.03 \text{ ft/sec.}$$

Run 3:

$$V = (85.49) (.84) (0.97) \sqrt{\frac{740}{(30.06)(24.03)}} = 70.50 \text{ ft/sec.}$$

$$Q_{sd} = 3600 \left[1 - B_{wc} \right] V_s A \left[\frac{T_{std}}{T_{stk}} \right] \left[\frac{P_s}{P_{std}} \right]$$

Where:

- Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, (dscf/hr).
- A = Cross sectional area of stack, (ft.²).
- 3600 = Conversion factor, (sec./hr.).
- t_s = Stack temperature, (°f).
- T_s = Absolute stack temperature, (°R).
- T_{std} = Standard absolute temperature, (528°R).
- P_{bar} = Barometric pressure at measurement site, (in.Hg.).
- P_g = Stack static pressure, (in.Hg.).
- P_s = Absolute stack gas pressure, (in.Hg.); = $P_{bar} + P_g$
- P_{std} = Standard absolute pressure, (29.92 in.Hg.).

Run 1:

$$Q_{sd} = 3600(1 - .4154)(66.90)(13.75) \left[\frac{528}{720} \right] \left[\frac{30.06}{29.92} \right] = 1426326.5 \frac{dscf}{hr}$$

Run 2:

$$Q_{sd} = 3600(1 - .4369)(67.03)(13.75) \left[\frac{528}{740} \right] \left[\frac{30.06}{29.92} \right] = 1339336.0 \frac{dscf}{hr}$$

Run 3:

$$Q_{sd} = 3600(1 - .4400)(70.50)(13.75) \left[\frac{528}{740} \right] \left[\frac{30.06}{29.92} \right] = 1400915.5 \frac{dscf}{hr}$$

$$E = \frac{(C_s) (Q_{sd})}{7000 \text{ gr./lb.}} = \text{lb. / hr.}$$

Where:

E = Emissions rate, lb/hr.

C_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr/dscf.

Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run 1:

$$E = \frac{(0.0067) (1426326.5)}{7000} = 1.37 \text{ lb. / hr.}$$

Run 2:

$$E = \frac{(0.0142) (1339336.0)}{7000} = 2.72 \text{ lb. / hr.}$$

Run 3:

$$E = \frac{(0.0133) (1400915.5)}{7000} = 2.66 \text{ lb. / hr.}$$

$$E = \frac{(C_s) (Q_{sd})}{7000 \text{ gr./lb.}} = \text{lb. / hr.}$$

Where:

E = Emissions rate, lb/hr.

C_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr/dscf.

Q_{sd} = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run 1:

$$E = \frac{(0.0024) (1426326.5)}{7000} = 0.49 \text{ lb. / hr.}$$

Run 2:

$$E = \frac{(0.0021) (1339336.0)}{7000} = 0.40 \text{ lb. / hr.}$$

Run 3:

$$E = \frac{(0.0013) (1400915.5)}{7000} = 0.26 \text{ lb. / hr.}$$

$$I = 100 T_s \left[\frac{0.002669 V_{ic} + \frac{(V_m / T_m) (P_{bar} + dH / 13.6)}{\Theta V_s P_s A_n}}{60} \right]$$

Where:

- I = Percent isokinetic sampling.
- 100 = Conversion to percent.
- T_s = Absolute average stack gas temperature, °R.
- 0.002669 = Conversion factor, Hg - ft³/ml - °R.
- V_{ic} = Ttl vol of liquid collected in impingers and silica gel, ml.
- T_m = Absolute average dry gas meter temperature, °R.
- P_{bar} = Barometric pressure at sampling site, (in. Hg).
- dH = Av pressure differential across the oriface meter, (in.H₂O).
- 13.6 = Specific gravity of mercury.
- 60 = Conversion seconds to minutes.
- Θ = Total sampling time, minutes.
- V_s = Stack gas velocity, ft./sec.
- P_s = Absolute stack gas pressure, in. Hg.
- A_n = Cross sectional area of nozzle, ft².

Run 1:

$$I = (100)(720) \left[\frac{(0.002669)(*****) + \frac{37.235}{564} \left[30.06 + \frac{1.29}{13.6} \right]}{60 (60.0) (66.90) (30.06) (.000341)} \right] = 96.3\%$$

Run 2:

$$I = (100)(740) \left[\frac{(0.002669)(*****) + \frac{41.834}{570} \left[30.06 + \frac{1.58}{13.6} \right]}{60 (60.0) (67.03) (30.06) (.000341)} \right] = 114.2\%$$

Run 3:

$$I = (100)(740) \left[\frac{(0.002669)(*****) + \frac{41.393}{575} \left[30.06 + \frac{1.51}{13.6} \right]}{60 (60.0) (70.50) (30.06) (.000341)} \right] = 107.0\%$$

$$\% E_a = \frac{100 \times (\% O_2) - 0.5 (\% CO)}{0.264 (\% N_2) - (\% O_2) + 0.5 (\% CO)}$$

- Where: %E_a = Percent excess air.
%O₂ = Percent oxygen by volume, dry basis.
%CO = Percent carbon monoxide by volume, dry basis.
%CO₂ = Percent carbon dioxide by volume, dry basis.
%N₂ = Percent nitrogen by volume, dry basis.

Run # 1:
$$\frac{100 \times (\% 8.70) - .05 (\% .00)}{0.264 (\% 82.10) - (\% 8.70) + 0.5 (\% .00)} = 67.1 \%$$

Run # 2:
$$\frac{100 \times (\% 5.00) - .05 (\% .00)}{0.264 (\% 87.30) - (\% 5.00) + 0.5 (\% .00)} = 27.7 \%$$

Run # 3:
$$\frac{100 \times (\% 3.20) - .05 (\% .00)}{0.264 (\% 92.80) - (\% 3.20) + 0.5 (\% .00)} = 15.0 \%$$

VII. CALCULATIONS
D. GASEOUS POLLUTANTS

NAME: LEHMAN ROBERTS (NAPA)
LOCATION: MEMPHIS, TENNESSEE

DATE: 9-03-91

TOTAL HYDROCARBON EMISSIONS: Convert ppm (wet) to ppm (dry)

$$\text{ppm}_d = \text{ppm}_w \left(\frac{100}{100 - B_{ws}} \right)$$

Where: ppm_d = Parts per million, dry basis.
 ppm_w = Parts per million, wet basis (as measured by the instrument).
 B_{ws} = Proportion of water vapor, by volume, in the gas stream.

Run #1:

$$\text{THC} = (124.4) \left(\frac{100}{100 - 46.21} \right) = 231.3 \text{ ppm}_d$$

Run #2:

$$\text{THC} = (143.6) \left(\frac{100}{100 - 43.03} \right) = 252.1 \text{ ppm}_d$$

Run #3:

$$\text{THC} = (192.2) \left(\frac{100}{100 - 42.63} \right) = 335.0 \text{ ppm}_d$$

NAME: LEHMAN ROBERTS (NAPA)
LOCATION: MEMPHIS, TENNESSEE

DATE: 9-03-91

TOTAL HYDROCARBON EMISSIONS: POUNDS PER HOUR

$$E = (2.59 \times 10^{-9}) (M_d) (\text{ppm}_d) (Q_{sd})$$

Where: E = Total Hydrocarbon emissions rate, lbs/hr.

2.59×10^{-9} = Conversion factor, lbs/dscf.

M_d = Dry molecular weight.

Q_{sd} = Dry volumetric stack gas flow rate corrected to std. conditions, dscf/hr.

ppm_d = Parts per million, dry basis.

Run #1:

$$E = (2.59 \times 10^{-9}) (16.04) (231.3) (1,254,491.3) = 12.05 \frac{\text{lbs}}{\text{hr}} \text{ as methane}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (16.04) (252.1) (1,410,621.9) = 14.77 \frac{\text{lbs}}{\text{hr}} \text{ as methane}$$

Run 3:

$$E = (2.59 \times 10^{-9}) (16.04) (335.0) (1,463,169.4) = 20.36 \frac{\text{lbs}}{\text{hr}} \text{ as methane}$$

NAME: LEHMAN ROBERTS (NAPA)
LOCATION: MEMPHIS, TENNESSEE

DATE: 9-03-91

TOTAL SO₂ EMISSIONS: POUNDS PER HOUR

$$E = (2.59 \times 10^{-9}) (M_d) (\text{ppm}_d) (Q_{sd})$$

Where: E = Sulfur dioxide emissions rate, lbs/hr.

2.59×10^{-9} = Conversion factor, lbs/dscf.

M_d = Dry molecular weight.

Q_{sd} = Dry volumetric stack gas flow rate corrected to std. conditions, dscf/hr.

ppm_d = Parts per million, dry basis.

Run #1:

$$E = (2.59 \times 10^{-9}) (64.07) (1.6) (1,254,491.3) = 0.33 \frac{\text{lbs}}{\text{hr}}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (64.07) (2.3) (1,410,621.9) = 0.54 \frac{\text{lbs}}{\text{hr}}$$

Run 3:

$$E = (2.59 \times 10^{-9}) (64.07) (2.0) (1,463,169.4) = 0.49 \frac{\text{lbs}}{\text{hr}}$$

NAME: LEHMAN ROBERTS (NAPA)
LOCATION: MEMPHIS, TENNESSEE

DATE: 9-03-91

TOTAL CARBON MONOXIDE EMISSIONS: POUNDS PER HOUR

$$E = (2.59 \times 10^{-9}) (M_d) (\text{ppm}_d) (Q_{sd})$$

Where: E = Carbon Monoxide emissions rate, lbs/hr.

2.59×10^{-9} = Conversion factor, lbs/dscf.

M_d = Dry molecular weight.

Q_{sd} = Dry volumetric stack gas flow rate corrected to std. conditions, dscf/hr.

ppm_d = Parts per million, dry basis.

Run #1:

$$E = (2.59 \times 10^{-9}) (28.01) (>1,000) (1,254,491.3) = >91.01 \frac{\text{lbs}}{\text{hr}}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (28.01) (>1,000) (1,410,621.9) = >102.33 \frac{\text{lbs}}{\text{hr}}$$

Run 3:

$$E = (2.59 \times 10^{-9}) (28.01) (>1,000) (1,463,169.4) = >106.15 \frac{\text{lbs}}{\text{hr}}$$

NAME: LEHMAN ROBERTS (NAPA)
LOCATION: MEMPHIS, TENNESSEE

DATE: 9-03-91

TOTAL NO_x EMISSIONS: LBS PER HOUR

$$E = (2.59 \times 10^{-9}) (M_d) (\text{ppm}_d) (Q_{sd})$$

Where: E = Nitrogen oxide emissions rate, lbs/hr.

2.59×10^{-9} = Conversion factor, lbs/dscf.

M_d = Dry molecular weight.

Q_{sd} = Dry volumetric stack gas flow rate corrected to std. conditions, dscf/hr.

ppm_d = Parts per million, dry basis.

Run #1:

$$E = (2.59 \times 10^{-9}) (46.01) (45.6) (1,254,491.3) = 6.82 \frac{\text{lbs}}{\text{hr}}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (46.01) (37.6) (1,410,621.9) = 6.32 \frac{\text{lbs}}{\text{hr}}$$

Run 3:

$$8E = (2.59 \times 10^{-9}) (46.01) (39.3) (1,463,169.4) = 6.85 \frac{\text{lbs}}{\text{hr}}$$

VIII. FIELD DATA

A. INSTRUMENTAL

LEHMAN ROBERTS

RUN # 1 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: LEHMAN ROBERTS

```

:.....:
CHAN NAME      HC      SO2      CO2      CO      O2      NOx
CHAN UNITS     ppm     ppm      %        ppm     %       ppm
FULL SCALE    1000.0  100.0    20.0    1000.0  25.0    100
ZERO OFFSET   0.0     0.0     0.0     0.0     0.0     0
START / CHANNEL 01      02      03      04      05      06
:.....:
09/03/91  11:25  99.5     0.8     7.2    1013.0   9.0     50
09/03/91  11:26  93.5     1.0     7.2    1023.5   8.7     48
09/03/91  11:27  95.5     1.1     7.3    1023.5   8.6     47
09/03/91  11:28  100.0    1.3     7.4    1023.5   8.5     48
09/03/91  11:29  98.5     1.3     7.3    1023.5   8.5     49
09/03/91  11:30  95.5     1.3     7.2    1023.5   8.7     48
09/03/91  11:31  95.0     1.2     7.3    1023.5   8.5     48
09/03/91  11:32  98.0     1.2     7.4    1023.5   8.3     48
09/03/91  11:33  107.0    1.3     7.5    1023.5   8.2     49
09/03/91  11:34  96.0     0.9     7.4    1023.5   8.3     49
09/03/91  11:35  103.5    1.1     7.5    1023.5   8.2     48
09/03/91  11:36  102.5    1.1     7.4    1023.5   8.2     48
09/03/91  11:37  108.0    1.2     7.4    1023.5   8.1     47
09/03/91  11:38  114.5    1.4     7.4    1023.5   7.9     45
09/03/91  11:39  110.0    1.4     7.5    1023.5   7.9     44
09/03/91  11:40  107.5    1.1     7.7    1023.5   7.8     47
09/03/91  11:41  87.5     1.2     7.8    1023.5   7.5     48
09/03/91  11:42  129.5    1.4     7.8    1023.5   7.2     46
09/03/91  11:43  103.5    1.3     7.8    1023.5   7.2     46
09/03/91  11:44  95.0     0.9     7.8    1023.5   7.5     50
09/03/91  11:45  102.0    1.1     7.8    1023.5   7.4     49
09/03/91  11:46  98.5     1.0     7.8    1023.5   7.5     49
09/03/91  11:47  103.0    1.0     7.8    1023.5   7.5     49
09/03/91  11:48  102.0    1.1     7.8    1023.5   7.4     49
09/03/91  11:49  115.5    1.0     7.7    1023.5   7.4     47
09/03/91  11:50  111.0    1.5     7.7    1023.5   7.3     45
09/03/91  11:51  105.0    1.0     7.7    1023.5   7.4     45
09/03/91  11:52  110.5    1.2     7.7    1023.5   7.3     46
09/03/91  11:53  102.0    0.8     7.8    1023.5   7.5     48
09/03/91  11:54  95.5     0.8     7.8    1023.5   7.5     49
09/03/91  11:55  112.0    1.0     7.8    1023.5   7.4     49
09/03/91  11:56  97.0     1.1     7.0    1023.5   8.2     45
09/03/91  11:57  90.0     0.8     7.3    1023.5   8.5     46
09/03/91  11:58  100.5    1.0     7.4    1023.5   8.2     47
09/03/91  11:59  371.0    4.9     7.3    1023.5   7.7     39
09/03/91  12:00  124.5    7.1     7.4    1023.5   7.4     35
09/03/91  12:01  221.5    2.7     7.4    1023.5   7.6     40
09/03/91  12:02  132.0    3.7     7.7    1023.5   7.3     38
09/03/91  12:03  176.0    2.9     8.0    1023.5   6.5     41
09/03/91  12:04  107.0    2.2     8.1    1023.5   6.4     43
09/03/91  12:05  111.5    1.0     8.1    1023.5   6.4     47
09/03/91  12:06  117.0    1.3     8.1    1023.5   6.3     45

```

LEHMAN ROBERTS

RUN # 1 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: LEHMAN ROBERTS

```

.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOx
CHAN UNITS         ppm          ppm          %            ppm          %            ppm
FULL SCALE        1000.0      100.0        20.0        1000.0      25.0        100
ZERO OFFSET       0.0         0.0         0.0         0.0         0.0         0
START / CHANNEL    01          02          03          04          05          06
.....
09/03/91 12:07  116.5      0.9        8.1        1023.5      6.5        48
09/03/91 12:08  125.0      0.9        8.2        1023.5      6.6        50
09/03/91 12:09  111.5      1.1        8.1        1023.5      6.3        46
09/03/91 12:10  124.5      1.7        8.0        1023.5      6.2        44
09/03/91 12:11  143.5      1.8        7.7        1023.5      6.8        42
09/03/91 12:12  138.0      1.9        7.7        1023.5      7.0        41
09/03/91 12:13  136.5      2.0        8.1        1023.5      6.5        43
09/03/91 12:14  137.0      1.5        8.1        1023.5      6.3        44
09/03/91 12:15  147.0      1.6        8.1        1023.5      6.3        44
09/03/91 12:16  139.0      1.9        8.1        1023.5      6.3        44
09/03/91 12:17  131.5      1.4        8.1        1023.5      6.4        46
09/03/91 12:18  218.5      2.6        8.0        1023.5      6.3        43
09/03/91 12:19  231.0      3.5        8.0        1023.5      6.1        38
09/03/91 12:20  136.0      2.8        8.0        1023.5      6.2        42
09/03/91 12:21  155.5      2.0        8.1        1023.5      6.2        43
09/03/91 12:22  158.0      2.2        8.1        1023.5      6.2        43
09/03/91 12:23  130.5      1.5        8.1        1023.5      6.3        45
09/03/91 12:24  131.0      1.3        8.1        1023.5      6.3        47
09/03/91 12:25  135.0      1.3        8.1        1023.5      6.3        46

Averages:         124.4      1.6        7.7 >1000.0      7.3        45.6

```

LEHMAN ROBERTS

RUN # 2 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: LEHMAN ROBERTS

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.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOx
CHAN UNITS         ppm          ppm          %            ppm          %            ppm
FULL SCALE        1000.0      100.0        20.0        1000.0      25.0        100
ZERO OFFSET       0.0         0.0          0.0         0.0         0.0         0
START / CHANNEL   01          02          03          04          05          06
.....
09/03/91 14:25 117.0      1.2         6.8        1023.5      8.8         39
09/03/91 14:26 116.0      1.3         6.7        1023.5      8.8         38
09/03/91 14:27 109.0      1.1         6.8        1023.5      8.7         38
09/03/91 14:28 129.0      1.4         6.7        1023.5      8.7         37
09/03/91 14:29 126.0      1.6         6.8        1023.5      8.7         36
09/03/91 14:30 124.5      1.4         6.8        1023.5      8.7         37
09/03/91 14:31 126.5      1.8         7.2        1023.5      8.1         38
09/03/91 14:32 135.0      1.7         7.2        1023.5      7.9         39
09/03/91 14:33 122.5      1.8         7.2        1023.5      7.9         38
09/03/91 14:34 133.0      1.7         7.2        1023.5      7.9         38
09/03/91 14:35 125.0      1.8         7.2        1023.5      7.9         39
09/03/91 14:36 115.5      1.6         7.1        1023.5      7.9         39
09/03/91 14:37 104.0      1.2         7.1        1023.5      8.1         40
09/03/91 14:38 126.0      1.3         7.2        1023.5      8.0         40
09/03/91 14:39 139.0      1.8         7.1        1023.5      8.0         38
09/03/91 14:40 126.5      1.5         7.1        1023.5      8.0         39
09/03/91 14:41 150.5      1.9         7.2        1023.5      7.9         38
09/03/91 14:42 151.0      2.4         7.1        1023.5      7.8         37
09/03/91 14:43 120.5      1.9         7.2        1023.5      7.9         38
09/03/91 14:44 126.5      1.8         7.2        1023.5      8.0         38
09/03/91 14:45 125.5      1.4         7.2        1023.5      7.9         39
09/03/91 14:46 109.5      1.3         7.2        1023.5      7.9         40
09/03/91 14:47 107.5      1.3         7.1        1023.5      7.9         39
09/03/91 14:48 111.0      1.0         7.2        1023.5      8.0         40
09/03/91 14:49  98.5      0.8         7.2        1023.5      8.1         42
09/03/91 14:50 108.0      1.1         7.2        1023.5      8.1         41
09/03/91 14:51 107.5      0.9         7.2        1023.5      8.1         41
09/03/91 14:52 102.5      0.7         7.1        1023.5      8.3         43
09/03/91 14:53 102.5      0.9         7.2        1023.5      8.3         44
09/03/91 14:54 163.0      1.6         7.2        1023.5      8.0         40
09/03/91 14:55 156.0      2.9         7.2        1023.5      7.8         36
09/03/91 14:56 127.5      1.5         7.2        1023.5      7.9         40
09/03/91 14:57 108.5      1.8         7.2        1023.5      7.9         38
09/03/91 14:58 129.5      2.0         7.1        1023.5      7.9         37
09/03/91 14:59 428.0      5.7         7.1        1023.5      7.8         34
09/03/91 15:00 452.0     14.0        7.0        1023.5      7.6         27
09/03/91 15:01 211.5      7.1         7.1        1023.5      7.7         30
09/03/91 15:02 144.5      2.8         7.1        1023.5      7.8         35
09/03/91 15:03 115.0      1.3         7.2        1023.5      7.9         38
09/03/91 15:04 118.5      1.5         7.2        1023.5      7.9         39
09/03/91 15:05 121.0      1.5         7.2        1023.5      7.9         39
09/03/91 15:06 146.0      2.0         7.2        1023.5      7.8         38
09/03/91 15:07 166.0      3.0         7.1        1023.5      7.7         36
.....

```


LEHMAN ROBERTS

RUN # 2 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: LEHMAN ROBERTS

```

.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOx
CHAN UNITS         ppm          ppm          %            ppm          %            ppm
FULL SCALE         1000.0      100.0        20.0         1000.0       25.0         100
ZERO OFFSET        0.0         0.0          0.0          0.0          0.0          0
START / CHANNEL    01          02          03          04          05          06
.....
09/03/91  15:08  142.0      2.6        7.1        1023.5       7.7         36
09/03/91  15:09  137.0      1.7        7.1        1023.5       7.8         38
09/03/91  15:10  156.0      2.3        7.1        1023.5       7.9         37
09/03/91  15:11  189.0      3.7        7.1        1023.5       7.7         35
09/03/91  15:12  160.0      3.3        7.1        1023.5       7.7         35
09/03/91  15:13  162.0      2.7        7.1        1023.5       7.7         36
09/03/91  15:14  151.0      3.3        7.1        1023.5       7.7         35
09/03/91  15:15  156.5      3.2        7.1        1023.5       7.7         35
09/03/91  15:16  133.5      2.8        7.2        1023.5       7.7         36
09/03/91  15:17  154.5      2.5        7.2        1023.5       7.6         37
09/03/91  15:18  213.0      3.6        7.2        1023.5       7.6         35
09/03/91  15:19  157.5      3.6        7.1        1023.5       7.6         34
09/03/91  15:20  144.0      2.6        7.1        1023.5       7.7         37
09/03/91  15:21  128.5      1.9        7.1        1023.5       7.8         38
09/03/91  15:22  117.0      1.9        7.1        1023.5       7.8         38
09/03/91  15:23  123.0      1.7        7.2        1023.5       7.8         38
09/03/91  15:24  134.0      1.8        7.2        1023.5       7.7         38
 9/03/91  15:25  120.5      2.0        7.2        1023.5       7.7         38

Averages:          143.6      2.3        7.1 >1000.0    7.9         37.6
    
```

VIII. FIELD DATA

B. GAS CHROMATOGRAPHY

FIELD ANALYSIS DATA SHEETS

Plant Lehman Roberts

Date 9-3-91

Location Mpls, TN

1. General Information:

Source temp. (°C)	<u>121</u>	Columnar temperature:	
Probe temp. (°C)	<u>121</u>	Initial (°C)/time (min)	<u>75</u>
Ambient temp. (°C)	<u>32</u>	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	<u>30.01</u>	Final (°C)/time (min)	<u>75</u>
Source press. (in. Hg)	<u> </u>	Carrier gas flow rate (ml/min)	<u>30</u>
Absolute source press. (mm)	<u> </u>	Detector temperature (°C)	<u> </u>
Sampling rate (liter/min)	<u>1</u>	Injection time (24-hr basis)	<u> </u>
Sample loop volume (ml)	<u>1</u>	Chart speed (mm/min)	<u> </u>
Sample loop temp. (°C)	<u>75</u>	Dilution ratio	<u> </u>
Dilution gas flow rate (ml/min)	<u> </u>	Dilution gas used (symbol)	<u> </u>

2. Field Analysis Data: 11:30 - 12:30

Run # 1A Time

<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>Methane</u>	<u> </u>	<u> </u>	<u> </u>	<u>BDL</u>
<u>B</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>T</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>

Run # 1B Time

<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>M</u>	<u> </u>	<u> </u>	<u> </u>	<u>BDL</u>
<u>B</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>T</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>

Run # 1C Time

<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>m</u>	<u>12.10</u>	<u>16</u>	<u>1153.6</u>	<u>13.8</u>
<u>B</u>	<u> </u>	<u> </u>	<u> </u>	<u>BDL</u>
<u>T</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>

FIELD ANALYSIS DATA SHEETS

Plant Behman Roberts Date 9-3-91

Location mph, TV

1. General Information:

Source temp. (°C) _____	Columnar temperature: _____
Probe temp. (°C) _____	Initial (°C)/time (min) _____
Ambient temp. (°C) _____	Program rate (°C/min) _____
Atmospheric press. (in. Hg) _____	Final (°C)/time (min) _____
Source press. (in. Hg) _____	Carrier gas flow rate (ml/min) _____
Absolute source press. (mm) _____	Detector temperature (°C) _____
Sampling rate (liter/min) _____	Injection time (24-hr basis) _____
Sample loop volume (ml) _____	Chart speed (mm/min) _____
Sample loop temp. (°C) _____	Dilution ratio _____
Dilution gas flow rate (ml/min) _____	Dilution gas used (symbol) _____

2. Field Analysis Data:

Run # 10 Time _____

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>Methane</u>	<u>181.36</u>	<u>16</u>	<u>2901.76</u>	<u>32.2</u>
<u>B</u>	_____	_____	_____	_____
<u>T</u>	_____	_____	_____	_____
<u>E</u>	_____	_____	_____	_____
<u>X</u>	_____	_____	_____	_____

Run # _____ Time _____

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

Run # _____ Time _____

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

FIELD ANALYSIS DATA SHEETS

Plant Lehman Roberts

Date 9-3-91

Location Mphs, TX

1. General Information:

Source temp. (°C)	<u>121</u>	Columnar temperature:	
Probe temp. (°C)	<u>121</u>	Initial (°C)/time (min)	<u>75</u>
Ambient temp. (°C)	<u>32</u>	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	<u>30.01</u>	Final (°C)/time (min)	<u>75</u>
Source press. (in. Hg)	<u> </u>	Carrier gas flow rate (ml/min)	<u>30</u>
Absolute source press. (mm)	<u> </u>	Detector temperature (°C)	<u> </u>
Sampling rate (liter/min)	<u>1</u>	Injection time (24-hr basis)	<u> </u>
Sample loop volume (ml)	<u>1</u>	Chart speed (mm/min)	<u> </u>
Sample loop temp. (°C)	<u>75</u>	Dilution ratio	<u> </u>
Dilution gas flow rate (ml/min)	<u> </u>	Dilution gas used (symbol)	<u> </u>

2. Field Analysis Data:

Run # 2A Time 14:17-15:17

<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>Methane</u>	<u> </u>	<u> </u>	<u> </u>	<u>BDL</u>
<u>B</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>T</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u>"</u>

Run # 2B Time

<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>m</u>	<u>93.62</u>	<u> </u>	<u> </u>	<u>16.6</u>
<u>B</u>	<u>4.04</u>	<u> </u>	<u> </u>	<u>.43</u>
<u>T</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>

Run # 2C Time

<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>m</u>	<u>24.71</u>	<u> </u>	<u> </u>	<u>4.3</u>
<u>B</u>	<u>7.34</u>	<u> </u>	<u> </u>	<u>.69</u>
<u>T</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>

FIELD ANALYSIS DATA SHEETS

Plant Belmont - Roberts

Date 9-3-91

Location Mpls, TD

1. General Information:

Source temp. (°C)	Columnar temperature:
Probe temp. (°C)	Initial (°C)/time (min)
Ambient temp. (°C)	Program rate (°C/min)
Atmospheric press. (in. Hg)	Final (°C)/time (min)
Source press. (in. Hg)	Carrier gas flow rate (ml/min)
Absolute source press. (mm)	Detector temperature (°C)
Sampling rate (liter/min)	Injection time (24-hr basis)
Sample loop volume (ml)	Chart speed (mm/min)
Sample loop temp. (°C)	Dilution ratio
Dilution gas flow rate (ml/min)	Dilution gas used (symbol)

2. Field Analysis Data:

Run # 20 Time _____

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>M</u>	<u>136.08</u>	<u>16</u>	<u>2177.28</u>	<u>24.2</u>
<u>B</u>	_____	_____	_____	_____
<u>T</u>	_____	_____	_____	_____
<u>E</u>	_____	_____	_____	_____
<u>X</u>	_____	_____	_____	_____

Run # _____ Time _____

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

Run # _____ Time _____

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

FIELD ANALYSIS DATA SHEETS

Plant Lehman Roberts Date 9-3-91

Location Mphs, TU

1. General Information:

Source temp. (°C)	<u>121</u>	Columnar temperature:	
Probe temp. (°C)	<u>121</u>	Initial (°C)/time (min)	<u>75</u>
Ambient temp. (°C)	<u>32</u>	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	<u>30.01</u>	Final (°C)/time (min)	<u>75</u>
Source press. (in. Hg)	<u> </u>	Carrier gas flow rate (ml/min)	<u>30</u>
Absolute source press. (mm)	<u> </u>	Detector temperature (°C)	<u> </u>
Sampling rate (liter/min)	<u>1</u>	Injection time (24-hr basis)	<u> </u>
Sample loop volume (ml)	<u>1</u>	Chart speed (mm/min)	<u> </u>
Sample loop temp. (°C)	<u>75</u>	Dilution ratio	<u> </u>
Dilution gas flow rate (ml/min)	<u> </u>	Dilution gas used (symbol)	<u> </u>

2. Field Analysis Data:

Run # 2A Time 16:30-17:30

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>Meth</u>	<u>62734</u>	<u>16</u>	<u>10037.44</u>	<u>111.7</u>
<u>B</u>	<u>13.46</u>	<u>16</u>	<u>215.36</u>	<u>1.2</u>
<u>I</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>F</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>

Run # 3B Time

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>M</u>	<u>144.85</u>	<u>16</u>	<u>2317.6</u>	<u>25.8</u>
<u>B</u>	<u>11.06</u>	<u>16</u>	<u>176.96</u>	<u>.98</u>
<u>I</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>

Run # 3C Time

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>M</u>	<u>2698</u>	<u>16</u>	<u>431.68</u>	<u>4.8</u>
<u>B</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>I</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>E</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>
<u>X</u>	<u> </u>	<u> </u>	<u> </u>	<u> </u>

FIELD ANALYSIS DATA SHEETS

Plant Lehman Roberts Date 9-3-91

Location Mphs, TN

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	_____
Probe temp. (°C)	_____	Initial (°C)/time (min)	_____
Ambient temp. (°C)	_____	Program rate (°C/min)	_____
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	_____
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	_____
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	_____	Injection time (24-hr basis)	_____
Sample loop volume (ml)	_____	Chart speed (mm/min)	_____
Sample loop temp. (°C)	_____	Dilution ratio	_____
Dilution gas flow rate (ml/min)	_____	Dilution gas used (symbol)	_____

2. Field Analysis Data:

Run # 3D Time _____

Components	Area	Attenuation	A x A Factor	Concentration (
<u>M</u>	<u>51.09</u>	<u>16</u>	<u>817.44</u>	<u>9.1</u>
<u>B</u>	<u>6.01</u>	<u>16</u>	<u>96.16</u>	<u>.58</u>
<u>T</u>	_____	_____	_____	_____
<u>E</u>	_____	_____	_____	_____
<u>X</u>	_____	_____	_____	_____

Run # _____ Time _____

Components	Area	Attenuation	A x A Factor	Concentration (
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

Run # _____ Time _____

Components	Area	Attenuation	A x A Factor	Concentration (
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

VIII. FIELD DATA

C. PAH'S

RAMCON ENVIRONMENTAL CORPORATION

Plant Lehman - Roberts

Location Memphis, TN

Operator C. C. Smith

Date 9-3-91

Run No. 1

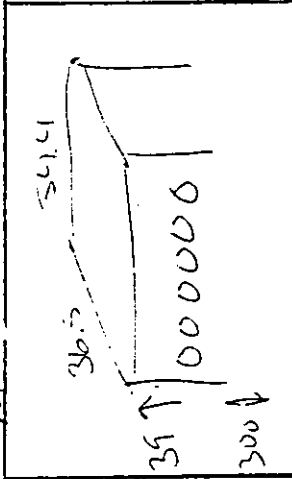
Sample Box No. 1

Meter Box No. C-124

Meter H @ 2.04

C Factor 1.97

Pitot Tube Coefficient Cp 0.84



Ambient Temperature 80

Barometric Pressure 30.01

Assumed Moisture, % 35

Probe Length, m(ft) 4.5

Nozzle Identification No. 0003409

Avg. Calibrated Nozzle Dia., (in.) 250/250/250

Probe Heater Setting 4

Leak Rate, m³/min. (cfm) 0.015 At 12

Probe Liner Material 35

Static Pressure, mm Hg (in. Hg) 1.01

Filter No. TH5511

WATER VOLUME, ml	SILICA GEL WEIGHT, g
FINAL 794	238
INITIAL 200	200
DIFFERENCE 594	38

Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Pg) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	11:26 11:28	4	255	.61	1.0	81.5 82.6	80	80	250	60
2	11:30	5	255	.64	1.1	83.9	110	92	250	60
3	11:32	5	255	.65	1.1	84.9	110	92	250	60
4	11:34	7	255	.75	1.3	86.1	114	92	250	60
5	11:36	7	255	.77	1.3	87.2	116	92	250	60
B 1	11:40 11:42	7	255	.65	1.1	88.2	110	94	250	60
2	11:44	7	255	.71	1.2	89.6	110	94	250	60
3	11:46	7	255	.78	1.3	90.5	108	94	250	60
4	11:48	7	255	.75	1.3	91.3	108	94	250	60
5	11:50	7	255	.60	1.0	92.3	108	94	250	60

RAMCON emissions test log sheet, cont. DATE 9-3-91 LOCATION MEMPHIS TA TEST NO. 1

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. HG)	STACK TEMP (°F)	VELOCITY HEAD (in. H ₂ O)	ORFICE DIFF. PRESSURE (in. H ₂ O)	GAS VOLUME (ft. ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
C 1	11:57 11:58	10	255	.73	1.2	93.2	104	94	250	60
2	11:57	10	255	.70	1.2	94.2	104	94	250	60
3	11:59	10	255	.85	1.4	95.2	104	94	250	60
4	12:01	10	255	.84	1.4	96.4	104	94	250	60
5	12:03	10	255	.79	1.3	97.8	104	94	250	60
D 1	12:05 12:07	10	255	.95	1.6	99.3	106	96	250	60
2	12:09	10	255	.95	1.6	101.0	106	96	250	60
3	12:11	10	255	.85	1.4	102.6	108	96	250	60
4	12:13	10	255	.83	1.4	103.9	108	96	250	60
5	12:15	10	255	.78	1.3	105.4	108	96	250	60
E 1	12:17 12:19	10	235	.82	1.4	106.5	110	96	250	60
2	12:21	10	255	.90	1.5	108.1	110	96	250	60
3	12:23	10	255	.85	1.4	109.5	112	96	250	60
4	12:25	10	255	.82	1.4	110.8	112	96	250	60
5	12:29	10	255	.75	1.3	112.1	112	96	250	60
F 1	12:28 12:30	10	255	.70	1.2	113.3	112	96	250	60
2	12:32	12	255	.98	1.7	114.4	114	96	250	60
3	12:34	12	255	1.0	1.7	116.2	114	96	250	60
4	12:36	12	255	.99	1.6	117.7	114	96	250	60
5	12:38	12	255	.95	1.6	119.176	114	96	250	60

Plant Lehigh Metals

M = 2.25 1.46

Location Memphis TN

Operator C. S. Clark

Date 9-3-91

Run No. 2 PAI's

Sample Box No. 1

Meter Box No. C-124

Meter H # 2.04

C Factor .77

Pitot Tube Coefficient Cp .84

Ambient Temperature 90

Barometric Pressure 30.01 FINAL 716 INITIAL 229

Assumed Moisture, % 45 INITIAL 200 DIFFERENCE 29

Probe Length, m(ft) 4 DIFFERENCE 516 29

Nozzle Identification No. 0003909

AVG. Calibrated Nozzle Dia., (in.) 2.0124/2.0

Probe Heater Setting 4

Leak Rate, m³/min. (cfm) 0.8712"

Probe Liner Material 7

Static Pressure, mm Hg (in. Hg) 1.01

Filter No. TH 5510

Schematic of Stack Cross Section

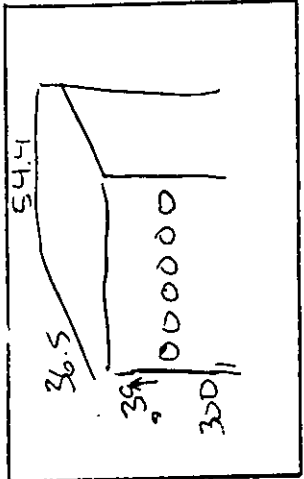
TRAV. PT. NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (T _s) °F	VELOCITY HEAD (P _g) in H ₂ O	PRESSURE DIFF. ORF. MTR in H ₂ O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	2:23 2:25	6	255	.65	.95	119.60 120.7	108	108	250	60
2	2:27	6	255	.70	1.0	121.8	116	108	250	60
3	2:29	7	255	.74	1.1	123.0	120	108	250	60
4	2:31	7	255	.76	1.1	124.1	122	108	250	60
5	2:33	7	255	.76	1.1	125.2	122	108	250	60
B 1	2:34 2:36	7	255	.70	1.0	126.4	122	108	250	60
2	2:38	7	255	.81	1.2	127.5	124	108	250	60
3	2:40	9	255	.91	1.3	128.8	124	108	250	60
4	2:42	10	255	.94	1.4	130.1	126	108	250	60
5	2:44	10	255	.79	1.2	131.4	126	108	250	60

RAMCON emissions test log sheet, cont. DATE: 9-3-71 LOCATION Microphos, Inc. TEST NO. 2

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP (°F)	VELOCITY HEAD (in. H ₂ O)	ORFICE DIFF. PRESSURE (in. H ₂ O)	GAS VOLUME (ft ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
C1	2:46 2:48	7	255	.70	1.0	132.6	122	110	250	60
2	2:50	8	255	.87	1.3	133.7	126	108	250	60
3	2:52	10	255	.95	1.4	135.0	128	108	250	60
4	2:54	10	255	.94	1.4	136.4	128	108	250	60
5	2:56	10	255	.77	1.1	137.6	128	108	250	60
D1	2:57 2:59	9	255	.95 ^{cc}	1.4	138.9	126	108	250	60
2	3:01	9	255	.95	1.4	140.3	128	108	250	60
3	3:03	11	255	1.0	1.5	141.7	128	108	250	60
4	3:05	11	255	1.1	1.6	143.0	128	108	250	60
5	3:07	11	255	.98	1.4	144.4	130	108	250	60
E1	3:08 3:10	10	255	.95	1.4	145.6	124	108	250	60
2	3:12	11	255	1.1	1.6	147.0	128	108	250	60
3	3:14	12	255	1.1	1.6	148.8	130	108	250	60
4	3:16	12	255	1.1	1.6	149.8	130	108	250	60
5	3:18	11 ^{cc}	255	.96	1.4	151.1	128	108	250	60
F1	3:20 3:22	9	255	.79	1.2	152.8	124	108	250	60
2	3:24	10	255	.79	1.2	154.1	128	108	250	60
3	3:26	11	255	1.1	1.6	154.9	128	108	250	60
4	3:28	12	255	1.1	1.6	156.3	128	108	250	60
5	3:30	12	255	1.1	1.6	157.7	128	108	250	60

RAMCON ENVIRONMENTAL CORPORATION

Plant Lehman Roberts
 Location Memphis TN
 Operator C. C. Cook
 Date 9-3-91
 Run No. 3
 Sample Box No. L
 Meter Box No. C-124
 Meter H @ 2.04
 C Factor 97
 Pitot Tube Coefficient Cp .84



Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (Ø) min.	VACUUM in. Hg	STACK TEMP (T _s) °F	VELOCITY HEAD (P _s) in H ₂ O	PRESSURE DIFF. ORF. MTR in H ₂ O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	4:38 4:40	7	255	1.1	1.6	157.8 159.3	110	110	250	60
2	4:42	7	255	1.1	1.6	160.8	122	108	250	60
3	4:44	7	255	.70	1.0	162.0	122	108	250	60
4	4:46	6	255	.72	1.1	163.2	124	108	250	60
5	4:48	7	255	.72	1.1	164.3	126	108	250	60
B 1	4:50 4:52	5	255	.75	1.1	165.4	122	108	250	60
2	4:54	5	255	.81	1.2	166.8	124	108	250	60
3	4:56	8	255	.94	1.4	168.0	128	108	250	60
4	4:58	9	255	.96	1.4	169.3	128	108	250	60
5	5:00	9	255	.94	1.4	170.7	128	108	250	60

Ambient Temperature 90
 Barometric Pressure 30.01
 Assumed Moisture, % 45
 Probe Length, m(ft) 4'
 Nozzle Identification No. 0003409
 Avg. Calibrated Nozzle Dia., (in.) 250/259.250
 Probe Heater Setting 4
 Leak Rate, m³/min. (cfm) 0.47/1.01
 Probe Liner Material SS
 Static Pressure, mm Hg (in. Hg) 1.01
 Filter No. _____

SPINDL. VOLUME, ml	MILICA GEL. WEIGHT, g
INITIAL	INITIAL
FINAL	FINAL
DIFFERENCE	DIFFERENCE

722
200
35

RAMCON emissions test log sheet, cont. DATE 9-3-71 LOCATION mph. Ta TEST NO. 3

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP (°F)	VELOCITY HEAD (in. H ₂ O)	ORIFICE DIFF. PRESSURE (in. H ₂ O)	GAS VOLUME V _m (ft. ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
1	5:03 5:03	8	255	.92	1.3	171.8	126	108	250	60
2	5:05	9	255	1.0	1.4	173.2	128	108	250	60
3	5:07	9	255	1.0	1.4	174.6	128	108	250	60
4	5:09	9	255	1.1	1.6	176.0	130	108	250	60
5	5:11	8	255	.80	1.2	177.3	132	108	250	60
D1	5:12 5:14	11	255	1.1	1.6	178.7	128	108	250	60
2	5:16	11	255	1.1	1.6	180.2	130	108	250	60
3	5:18	9	255	.87	1.3	181.4	130	108	250	60
4	5:20	9	255	.85	1.2	182.8	132	108	250	60
5	5:22 5:22	7	255	.64	.93	183.8	132	108	250	60
E1	5:23 5:25	10	255	1.0	1.4	185.2	128	108	250	60
2	5:27	10	255	1.1	1.6	186.5	130	108	250	60
3	5:29	11	255	1.1	1.6	187.9	132	108	250	60
4	5:31	11	255	1.1	1.6	189.5	132	108	250	60
5	5:33	10	255	.91	1.3	190.7	132	108	250	60
F1	5:34 5:36	8	255	1.1	1.6	192.2	128	108	250	60
2	5:38	11	255	1.1	1.6	193.6	130	108	250	60
3	5:40	11	255	1.1	1.6	194.7	132	108	250	60
4	5:42	11	255	1.1	1.6	196.2	132	108	250	60
5	5:44	11	255	1.0	1.4	197.5	132	108	250	60

FAH's

Behman - Loberk
Company Name

9-3-91
Date

REFERENCE METHOD 3: GAS ANALYSIS BY FYRITE

FUEL	F _o FACTORS
WOOD	1.0540
BARK	1.0830
ANTHRACITE	1.0699
BITUMINOUS	1.1398
LIGNITE	1.0761
OIL	1.3465
GAS	1.7489
PROPANE	1.5095
BUTANE	1.4791

O₂% = 20.9 - [F_o x CO₂%]

RUN #1: _____ = 20.9 - [_____ x _____]

RUN #2: _____ = 20.9 - [_____ x _____]

RUN #3: _____ = 20.9 - [_____ x _____]

RUN 1:	CO _{2x} <u>10</u>	CO _{2x} <u>8</u>	CO _{2x} <u>8</u>	AVG. <u>8.7</u>
	O _{2x} <u>5</u>	O _{2x} <u>5</u>	O _{2x} <u>4</u>	AVG. <u>4.7</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>86.6</u>
RUN 2:	CO _{2x} <u>8</u>	CO _{2x} <u>7</u>	CO _{2x} <u>7</u>	AVG. <u>7.3</u>
	O _{2x} <u>6</u>	O _{2x} <u>5</u>	O _{2x} <u>6</u>	AVG. <u>5.7</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>87.0</u>
RUN 3:	CO _{2x} <u>8</u>	CO _{2x} <u>8</u>	CO _{2x} <u>7</u>	AVG. <u>7.7</u>
	O _{2x} <u>5</u>	O _{2x} <u>5</u>	O _{2x} <u>5</u>	AVG. <u>5.0</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>87.3</u>

VIII. FIELD DATA

D. FORMALDEHYDE

Plant LEIGHMAN ROBERTS

FORMALDEHYDE

Location MEMPHIS, TN

Operator W. J. LOCKETT

Date 9-30-80

Run No. 1

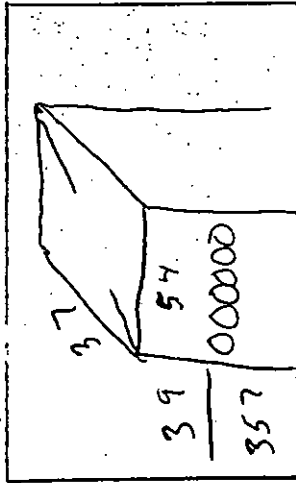
Sample Box No. 1

Meter Box No. C-185

Meter H @ 1.417

C Factor 1.011

Pitot Tube Coefficient Cp .84



Ambient Temperature 72
 Barometric Pressure 30.15 FINAL 549.7
 Assumed Moisture, % 30 INITIAL 200
 Probe Length, m(ft) 4' DIFFERENCE 4/16
 Nozzle Identification No. 10003976
 Avg. Calibrated Nozzle Dia., (in.) 270/270/270
 Probe Heater Setting 7
 Leak Rate, m³/min. (cfm) 1005 @ 10"
 Probe Liner Material GLASS
 Static Pressure, mm Hg (in. Hg) N.A.
 Filter No. N.A.

Schematic of Stack Cross Section

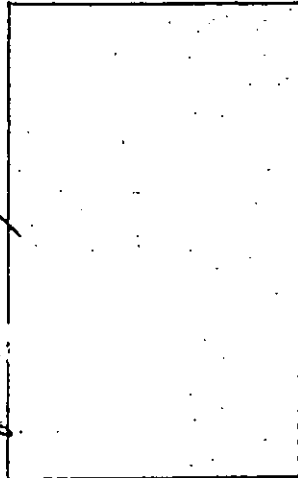
TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	10:56 10:59	2	235	.55	1.1	889.0 890.9	72	72	260	55
2	11:02	2	235	.67	1.3	893.1	90	74	260	55
3	11:05	2	235	.63	1.2	895.1	96	74	260	55
4	11:08	2	230	.50	.99	897.2	100	74	260	55
B 1	11:09:30 11:11:30	2	235	.75	1.5	899.3	96	76	260	55
2	11:15:30	2	240	.72	1.4	901.6	104	76	260	55
3	11:18:30	2	235	.65	1.3	903.7	106	78	260	55
4	11:21:30	2	235	.51	1.0	905.5	108	78	260	55
C 1	11:23 11:26	2	235	.57	1.1	907.5	102	78	260	55
2	11:29	2	235	.77	1.5	909.8	108	80	260	55
3	11:32	2	235	.63	1.2	911.9	110	80	260	55
4	11:35	2	235	.50	.98	913.8	112	80	260	55

Plant Leiman Roberts

Formaldehyde

Ambient Temperature 86

NO. OF REACTOR HEIGHT. 630



Location Memphis, TN

Operator W.J. Lockert

Date 9-30-91

Run No. 1

Sample Box No. 1

Meter Box No. C-181

Meter Hg 1.417

C Factor 1.011

Pitot Tube Coefficient Cp 0.88

Barometric Pressure 30.15 FINAL

Assumed Moisture, % 30 INITIAL

Probe Length, m(ft) 4 DIFFERENCE

Nozzle Identification No. 20.5

Avg. Calibrated Nozzle Dia., (in.) 7

Probe Heater Setting CLASS

Leak Rate, m³/min. (cfm) 1,000.25

Probe Liner Material CLASS

Static Pressure, mm Hg (in. Hg) 1.09

Filter No. 1.09

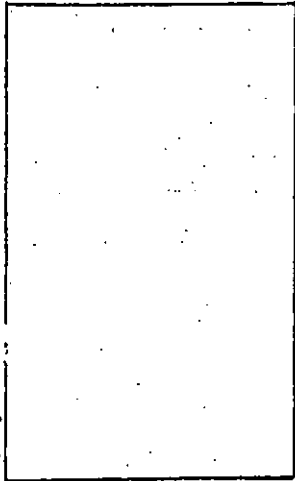
Schematic of Stack Cross Section

TRAV. PT. NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR. in. H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	13:42 / 13:45	2	250	.61	1.2	941.5 / 943.6	84	84	260	55
2	13:48	2	255	.56	1.1	945.6	104	86	260	55
3	13:51	2	255	.60	1.2	947.7	110	86	260	55
4	13:54	2	250	.62	1.2	949.8	112	86	260	55
B 1	13:55 / 13:58	2	245	.61	1.2	951.9	110	86	260	55
2	14:01	2	250	.69	1.4	954.1	116	86	260	55
3	14:04	2	250	.67	1.3	956.3	116	86	260	55
4	14:07	2	250	.63	1.2	958.5	116	56	260	55
C 1	14:09 / 14:11	2	245	.75	1.5	960.8	104	86	260	55
2	14:14	2	255	.72	1.4	963.1	118	86	260	55
3	14:17	2	250	.67	1.3	965.2	118	88	260	55
4	14:20	2	250	.62	1.2	967.3	120	88	260	55

Plant Leiman Roberts

Form AL04040E

Ambient Temperature 89
 Barometric Pressure 30.15
 Assumed Moisture, % 70
 Probe Length, m(ft) 4'
 Nozzle Identification No. 274
 Avg. Calibrated Nozzle Dia., (in.) 2.70/2.74/2.70
 Probe Heater Setting
 Leak Rate, m³/min. (cfm) 6.655
 Probe Liner Material
 Static Pressure, mm Hg (in. Hg)
 Filter No. 24



Location Memphis, TN
 Operator W. J. Locke
 Date 9-30-91
 Run No. 3
 Sample Box No. 1
 Meter Box No. C-185
 Meter H_e 1.417
 C Factor 1.011
 Pitot Tube Coefficient Cp .84

Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (θ)min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	16:13 / 16:16	2	240	.61	1.2	000.2 / 2.3	92	92	260	60
2	16:19	2	240	.70	1.4	4.6	108	92	260	60
3	16:22	2	240	.59	1.2	6.7	114	92	260	60
4	16:25	2	240	.47	1.3	8.6	116	92	260	60
B 1	16:26 / 16:29	2	240	.75	1.5	10.9	112	92	260	60
2	16:32	2	240	.79	1.6	13.3	118	92	260	60
3	16:35	2	240	.64	1.3	15.6	120	92	260	60
4	16:38	2	240	.50	1.1	17.5	120	92	260	60
C 1	16:39 / 16:42	2	240	.78	1.5	19.8	116	92	260	60
2	16:45	2	245	.75	1.5	22.2	120	92	260	60
3	16:48	2	245	.60	1.2	24.3	120	92	260	60
4	16:51	2	245	.49	1.1	26.2	120	92	260	60

Lehman Roberts
Company Name

9/30/21
Date

REFERENCE METHOD 3: GAS ANALYSIS BY FYRITE

FUEL	F _o FACTORS
WOOD	1.0540
BARK	1.0830
ANTHRACITE	1.0699
BITUMINOUS	1.1398
LIGNITE	1.0761
OIL	1.3465
GAS	1.7489
PROPANE	1.5095
BUTANE	1.4791

$O_2\% = 20.9 - [F_o \times CO_2\%]$

RUN #1: _____ = 20.9 - [_____ x _____]

RUN #2: _____ = 20.9 - [_____ x _____]

RUN #3: _____ = 20.9 - [_____ x _____]

RUN 1:	CO _{2x} <u>3.5</u>	CO _{2x} <u>1</u>	CO _{2x} <u>1.5</u>	AVG. <u>2.0</u>
	O _{2x} <u>14.8</u>	O _{2x} <u>19.2</u>	O _{2x} <u>18.3</u>	AVG. <u>17.4</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>80.6</u>

RUN 2:	CO _{2x} <u>6</u>	CO _{2x} <u>4</u>	CO _{2x} <u>3</u>	AVG. <u>4.3</u>
	O _{2x} <u>10.4</u>	O _{2x} <u>13.9</u>	O _{2x} <u>15.6</u>	AVG. <u>13.3</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>82.4</u>

RUN 3:	CO _{2x} <u>3</u>	CO _{2x} <u>2</u>	CO _{2x} <u>1.5</u>	AVG. <u>2.2</u>
	O _{2x} <u>15.6</u>	O _{2x} <u>17.4</u>	O _{2x} <u>18.3</u>	AVG. <u>17.1</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>80.7</u>

VIII. FIELD DATA

E. PARTICULATE & CONDENSIBLE PM

Plant Lehman-Roberts

Location Memphis TN

Operator C. Crank

Date 9-9-91

Run No. 1

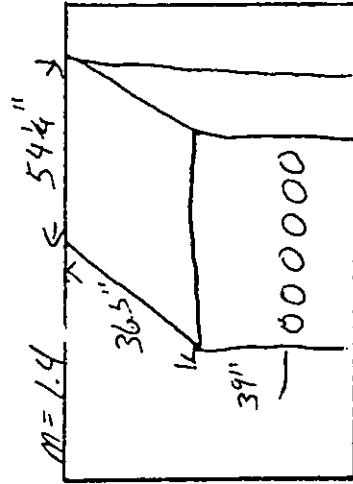
Sample Box No. C-124

Meter Box No. 2.09

Meter H_e 97

C Factor 84

Pitot Tube Coefficient Cp 84



Schematic of Stack Cross Section

Ambient Temperature 75
 Barometric Pressure 30.06
 Assumed Moisture, % 86
 Probe Length, m(ft) 3.00
 Nozzle Identification No. 0203407
 Avg. Calibrated Nozzle Dia., (in.) 25.125
 Probe Heater Setting 4
 Leak Rate, m³/min. (cfm) 0.475
 Probe Liner Material Cr655
 Static Pressure, mm Hg (in. Hg) 4.01
 Filter No. P15469

TRAV. PT NO.	SAMPLING TIME (9) min.	VACUUM in. Hg	STACK TEMP (T _S) °F	VELOCITY HEAD (P _S) in H ₂ O	PRESSURE DIFF. ORF. MTR in H ₂ O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	9:52 9:54	1	260	88	98.12	187 200.0	86	86	250	60
A 2	9:56	1	260	86	1.2	201.2	100	86	250	60
A 3	9:58	1	260	77	1.1	202.5	102	86	250	60
A 4	10:00	1	260	60	.84	203.3	104	86	250	60
A 5	10:02	1	260	63	.88	204.3	106	86	250	60
B 1	10:03 10:05	1	260	84	1.2	205.5	104	88	250	60
B 2	10:07	1	260	90	1.3	206.7	108	88	250	60
B 3	10:09	1	260	88	1.2	207.9	110	88	250	60
B 4	10:11	1	260	89	1.2	209.1	114	90	250	60
B 5	10:13	1	260	80	1.1	210.2	114	90	250	60

RAMCON emissions test log sheet, cont. DATE 9-4-11 LOCATION Mcropolis T₂ TEST NO. /

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP (°F)	VELOCITY HEAD (in. H ₂ O)	ORIFICE DIFF. PRESSURE (in. H ₂ O)	GAS VOLUME (ft ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
C1	10:14 10:16	1	260	.91	1.3	211.5	112	92	250	60
2	10:18	1	260	.90	1.3	212.7	114	92	250	60
3	10:20	1	260	.94	1.3	214.0	116	92	250	60
4	10:22	2	260	.98	1.4	215.3	118	92	250	60
5	10:24	2	260	1.0	1.4	216.6	120	92	250	60
D1	10:25 10:27	2	260	1.1	1.6	217.9	116	94	250	60
2	10:29	2	260	1.1	1.6	219.4	118	94	250	60
3	10:31	2	260	.73	1.0	220.5	120	94	250	60
4	10:33	2	260	.78	1.1	221.7	120	94	250	60
5	10:35	2	260	.78	1.1	222.9	120	94	250	60
E1	10:36 10:38	2	260	.89	1.2	224.3	118	96	250	60
2	10:40	2	260	.91	1.3	225.4	120	96	250	60
3	10:42	2	260	.98	1.4	226.6	122	96	250	60
4	10:44	2	260	1.0	1.4	228.0	122	96	250	60
5	10:46	2	260	1.0	1.4	229.2	122	96	250	60
F1	10:47 10:49	2	260	.96	1.3	230.4	118	98	250	60
2	10:51	2	260	1.0	1.4	231.7	122	98	250	60
3	10:53	2	260	1.2	1.7	233.2	122	98	250	60
4	10:55	2	260	1.1	1.6	234.5	124	98	250	60
5	10:57	2	260	1.1	1.6	235.935	124	98	250	60

RAMCON ENVIRONMENTAL CORPORATION

Plant Lehrman Roberts

Location Memphis TN
 Operator C. C. Cobb
 Date 9-4-91
 Run No. 2
 Sample Box No. 1
 Meter Box No. 1
 Meter H @ 2.04
 C Factor .91
 Pitot Tube Coefficient Cp .84



Ambient Temperature 80
 Barometric Pressure 30.06 FINAL 81.5
 Assumed Moisture, % 40 INITIAL 300
 Probe Length, m (ft) 4 DIFFERENCE 575
 Nozzle Identification No. 0003407
 Avg. Calibrated Nozzle Dia., (in.) 0.25125
 Probe Heater Setting 4
 Leak Rate, m³/min. (cfm) 0.112
 Probe Liner Material 6.655
 Static Pressure, mm Hg (in. Hg) 1.01
 Filter No. PT5467

NO. OF VOLUMES 81.5
 WGT. 230

Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (Ø) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	11:45 11:45	2	280	.55	.99	236.4 237.4	100	100	250	60
A 2	11:47	4	280	.75	1.4	238.5	110	100	250	60
A 3	11:49	5	280	.96	1.7	240.0	114	98	250	60
A 4	11:51	5	280	.89	1.6	241.4	116	98	250	60
A 5	11:53	5	280	.98	1.8	243.0	120	98	250	60
B 1	11:54 11:56	5	280	.94	1.7	244.5	116	98	250	60
B 2	11:58	5	280	.91	1.6	245.8	120	98	250	60
B 3	12:00	5	280	1.0	1.8	247.3	122	98	250	60
B 4	12:02	5	280	1.0	1.8	248.9	122	98	250	60
B 5	12:04	5	280	.87	1.6	250.2	122	98	250	60

RAMCO emissions test log sheet, cont. DATE 9-4-91 LOCATION *Phys. Tr.* TEST NO. 2

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP (°F)	VELOCITY HEAD (in. H ₂ O)	ORFICE DIFF. PRESSURE (in. H ₂ O)	GAS VOLUME V _m (ft. ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
C 1	12:05 12:07	5	280	.91	1.6	251.2	118	98	250	60
2	12:09	5	280	.75	1.4	253.0	122	98	250	60
3	12:11	5	280	.86	1.5	254.6	122	98	250	60
4	12:13	5	280	1.0	1.8	255.8	124	98	250	60
5	12:15	5	280	1.0	1.8	257.3	124	98	250	60
D 1	12:16 12:16	4	280	.83	1.5	258.9	120	100	250	60
2	12:20	4	280	.83	1.5	260.2	122	98	250	60
3	12:22	4	280	.84	1.5	261.3	124	98	250	60
4	12:24	4	280	.72	1.3	262.7	124	98	250	60
5	12:26	4	280	.61	1.1	263.9	124	98	250	60
E 1	12:27 12:29	5	280	.92	1.7	265.3	120	98	250	60
2	12:31	5	280	.88	1.6	266.7	124	98	250	60
3	12:33	5	280	.77	1.4	268.1	124	100	250	60
4	12:35	5	280	.71	1.3	269.4	126	100	250	60
5	12:37	5	280	.60	1.1	270.6	126	100 ^{59/8}	250	60
F 1	12:38 12:40	7	280	1.1	2.0	272.3	120	100	250	60
2	12:42	6	280	1.0	1.8	273.9	124	100	250	60
3	12:44	6	280	1.0	1.8	275.4	126	100	250	60
4	12:46	4	280	1.0	1.8	276.7	126	100	250	60
5	12:48	6	280	1.0	1.8	278.2	126	100	250	60

Plant Lehman - Roberts

Location Memphis In.

Operator C. C. Cook

Date 9-4-91

Run No. 3

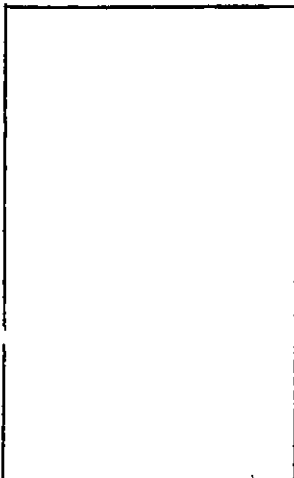
Sample Box No. 1

Meter Box No. C-124

Meter H e 2.04

C Factor .97

Pitot Tube Coefficient Cp .84



Ambient Temperature 85
 Barometric Pressure 30.06
 Assumed Moisture, % 40
 Probe Length, m(ft) 4
 Nozzle Identification No. 000907
 Avg. Calibrated Nozzle Dia., (in.) 25/32
 Probe Heater Setting 4
 Leak Rate, m³/min. (cfm) 0.16
 Probe Liner Material glass
 Static Pressure, mm Hg (in. Hg) 1.01
 Filter No. P15462

MPH	VOLUME	MPH DEL
FINAL	890	230
INITIAL	300	200
DIFFERENCE	590	30

Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Pg) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft ³	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A 1	1:29 1:31	3	280	1.0	1.6	278.500 279.8	110	110	250	60
2	1:33	3	280	1.2	1.9	281.4	118	106	250	60
3	1:35	3	280	1.1	1.8	282.8	122	104	250	60
4	1:37	3	280	1.0	1.6	284.3	124	104	250	60
5	1:39	3	280	1.1	1.6	285.7	124	104	250	60
B 1	1:40 1:42	3	280	1.1	1.8	287.2	122	104	250	60
2	1:44	3	280	1.1	1.8	288.7	124	104	250	60
3	1:46	3	280	1.1	1.8	290.2	124	104	250	60
4	1:48	3	280	1.0	1.6	291.8	126	104	250	60
5	1:50	3	280	1.2	1.5	293.0	128	104	250	60
								2270		

RAMCON emissions test log sheet, cont. DATE: 9-4-91 LOCATION Memphis Tn. TEST NO. 3

TRAVERSE POINT	SAMPLING TIME (min)	VACUUM (in. Hg)	STACK TEMP (°F)	VELOCITY HEAD ΔP_s (in. H ₂ O)	ORFICE DIFF. PRESSURE ΔH (in. H ₂ O)	GAS VOLUME V_m (ft. ³)	GAS SAMPLE TEMP. (°F)		SAMPLE BOX TEMP. (°F)	IMPINGER TEMP (°F)
							in	out		
C 1	1:51 1:53	3	280	.92	1.5	294.5	122	104	250	60
2	1:55	3	280	.92	1.5	295.9	126	104	250	60
3	1:57	3	280	1.0	1.6	297.4	128	104	250	60
4	1:59	3	280	1.0	1.6	299.2	128	104	250	60
5	2:01	3	280	1.0	1.6	300.0	128	104	250	60
D 1	2:02 2:04	3	280	.90	1.4	301.4	124	104	250	60
2	2:06	3	280	.85	1.4	302.9	128	104	250	60
3	2:08	3	280	.84	1.3	303.9	130	104	250	60
4	2:10	3	280	.74	1.2	305.2	130	104	250	60
5	2:12	3	280	.74	1.2	306.5	130	104	250	60
E 1	2:13 2:15	3	280	.95	1.5	307.9	126	104	250	60
2	2:17	3	280	.95	1.5	309.2	128	104	250	60
3	2:19	3	280	.88	1.4	310.5	130	104	250	60
4	2:21	3	280	.80	1.3	312.0	130	104	250	60
5	2:23	3	280	.79	1.3	313.2	130	104	250	60
F 1	2:24 2:26	3	280	.88	1.4	314.6	126	104	250	60
2	2:28	4	280	.94	1.5	315.9	128	104	250	60
3	2:30	3	280	.88	1.4	317.3	130	104	250	60
4	2:32	3	280	.85	1.4	318.5	130	104	250	60
5	2:34	3	280	.81	1.3	319.9	130	104	250	60

Lehman - Roberts

9-4-91

Company Name

Date

REFERENCE METHOD 3: GAS ANALYSIS BY FYRITE

FUEL

F_o FACTORS

WOOD	1.0540
BARK	1.0830
ANTHRACITE	1.0699
BITUMINOUS	1.1398
LIGNITE	1.0761
OIL	1.3465
GAS	1.7489
PROPANE	1.5095
BUTANE	1.4791

O₂% = 20.9 - [F_o x CO₂%]

RUN #1: _____ = 20.9 - [_____ x _____]

RUN #2: _____ = 20.9 - [_____ x _____]

RUN #3: _____ = 20.9 - [_____ x _____]

RUN 1:	CO _{2x} <u>9</u>	CO _{2x} <u>9</u>	CO _{2x} <u>9.5</u>	AVG. <u>9.2</u>
	O _{2x} <u>8</u>	O _{2x} <u>9</u>	O _{2x} <u>9</u>	AVG. <u>8.7</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>82.1</u>
RUN 2:	CO _{2x} <u>7</u>	CO _{2x} <u>8</u>	CO _{2x} <u>8</u>	AVG. <u>7.7</u>
	O _{2x} <u>4</u>	O _{2x} <u>5.5</u>	O _{2x} <u>5.5</u>	AVG. <u>5.0</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>87.3</u>
RUN 3:	CO _{2x} <u>4</u>	CO _{2x} <u>4</u>	CO _{2x} <u>4</u>	AVG. <u>4.0</u>
	O _{2x} <u>3</u>	O _{2x} <u>3.5</u>	O _{2x} <u>3</u>	AVG. <u>3.2</u>
	N _{2x} _____	N _{2x} _____	N _{2x} _____	AVG. <u>92.8</u>

IX. CALIBRATIONS

A. PAH DATA

int
INITIAL CALIBRATION CHECK

DATE : 25-Sep

NB
9-26-91

TIME : 15

DO
9-26-91

LAB FILE ID: RF20 =FE905 RF50 =FE901 RF80 =FE904
 RF120=FE903 RF160=FE902

COMPOUND	FLAG	RF 20NG	RF 50NG	RF 80NG	RF 120NG	RF 160NG	RF MEAN	%RSD
3 Naphthalene		1.036	0.941	0.976	0.989	0.965	0.981	3.6
4 2-Methylnaphthalene		0.812	0.794	0.802	0.812	0.858	0.816	3.0
6 2-Chloronaphthalene		0.940	0.924	0.915	0.901	0.856	0.907	3.5
7 Acenaphthylene		1.580	1.540	1.548	1.564	1.552	1.556	1.0
8 Acenaphthene	C	1.048	0.978	1.024	1.002	0.978	1.006	3.0
9 Fluorene		1.219	1.142	1.146	1.126	1.101	1.147	3.8
11 Phenanthrene		0.931	0.867	0.882	0.879	0.837	0.879	3.9
12 Anthracene		0.928	0.872	0.858	0.893	0.830	0.876	4.2
13 Fluoranthene	C	1.512	1.300	1.324	1.352	1.224	1.342	7.9
16 Pyrene		1.051	1.162	1.011	0.856	0.895	0.995	12.4
17 Benzo(a)anthracene		1.015	1.099	1.048	1.086	1.061	1.062	3.3
18 Chrysene		1.079	1.018	1.026	0.985	0.941	1.010	5.3
20 Benzo(b)fluoranthene		0.993	0.974	1.028	1.130	1.225	1.070	9.9
21 Benzo(k)fluoranthene		1.163	1.193	1.007	0.923	0.708	0.999	19.7
22 Benzo(e)pyrene		0.953	0.975	0.946	0.968	0.979	0.964	1.5
23 Benzo(a)pyrene	C	0.958	1.023	0.977	0.991	0.911	0.972	4.3
24 Perylene		0.659	0.580	0.567	0.568	0.557	0.586	7.1
25 Indeno(1,2,3-cd)pyrene		0.530	0.810	0.875	0.952	0.934	0.820	20.9
26 Dibenz(a,h)anthracene		0.642	0.843	0.942	0.985	0.973	0.877	16.3
27 Benzo(g,h,i)perylene		0.745	0.921	0.973	0.975	0.905	0.904	10.4
28 Pentachlorophenol	C	0.063	0.121	0.129	0.137	0.119	0.114	25.6
=====								
15 Terphenyl-d14	S	0.778	0.818	0.791	0.674	0.631	0.738	11.0
29 Nitrobenzene-d5	S	0.528	0.492	0.539	0.536	0.439	0.507	8.3
30 2-Fluorobiphenyl	S	0.927	0.864	0.860	0.824	0.772	0.850	6.7
31 2,4,6-Tribromophenol	S	0.127	0.111	0.162	0.154	0.115	0.134	17.4
32 Phenol-d5	S	1.530	1.588	1.731	1.725	1.513	1.617	6.5
33 Pyrene-d10	S	0.788	0.871	0.810	0.701	0.683	0.771	10.3
34 Anthracene-d10	S	0.954	0.880	0.889	0.900	0.837	0.892	4.7
35 1,4-Dibromobenzene-d4	S	0.783	0.619	0.776	0.715	0.574	0.693	13.5
36 1,3,5-Trichlorobenzene-d3	S	0.290	0.256	0.281	0.275	0.241	0.269	7.5

9/26
DAILY CALIBRATION CHECK

DATE : 25-Sep

TIME : 1

DB
9-26-91

DO
9-26-91

LAB FILE ID: FE901

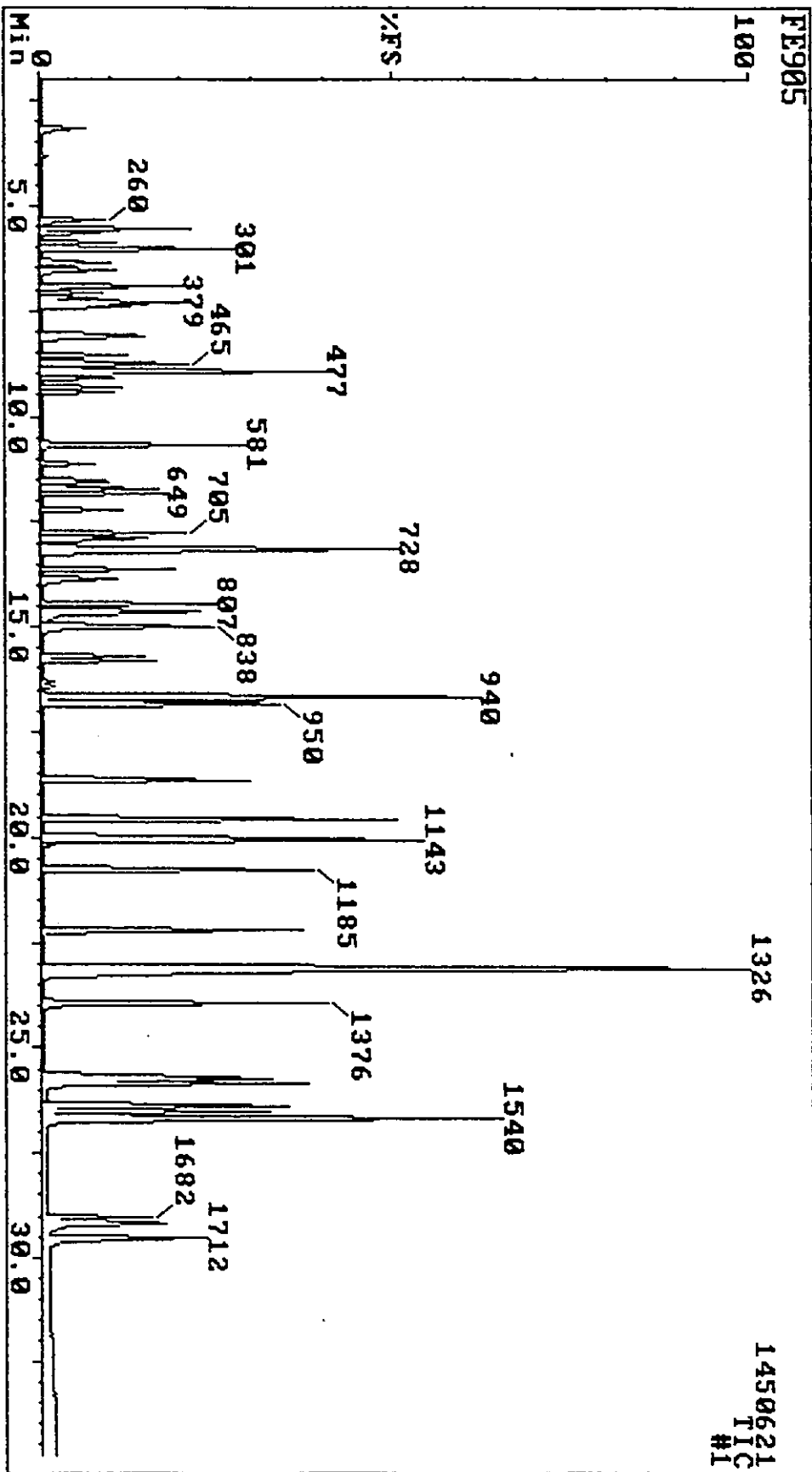
COMPOUND	FLAG	RF MEAN	RF 50	%D
3 Naphthalene		0.981	0.941	4.1
4 2-Methylnaphthalene		0.816	0.794	2.6
6 2-Chloronaphthalene		0.907	0.924	-1.8
7 Acenaphthylene		1.556	1.540	1.1
8 Acenaphthene	C	1.006	0.978	2.8
9 Fluorene		1.147	1.142	0.4
11 Phenanthrene		0.879	0.867	1.4
12 Anthracene		0.876	0.872	0.4
13 Fluoranthene	C	1.342	1.300	3.1
16 Pyrene		0.995	1.162	-16.8
17 Benzo(a)anthracene		1.062	1.099	-3.5
18 Chrysene		1.010	1.018	-0.8
20 Benzo(b)fluoranthene		1.070	0.974	9.0
21 Benzo(k)fluoranthene		0.999	1.193	-19.4
22 Benzo(e)pyrene		0.964	0.975	-1.1
23 Benzo(a)pyrene	C	0.972	1.023	-5.2
24 Perylene		0.586	0.580	1.0
25 Indeno(1,2,3-cd)pyrene		0.820	0.810	1.2
26 Dibenz(a,h)anthracene		0.877	0.843	3.9
27 Benzo(g,h,i)perylene		0.904	0.921	-1.9
28 Pentachlorophenol	C	0.114	0.121	-5.8
=====				
15 Terphenyl-d14	S	0.738	0.818	-10.8
29 Nitrobenzene-d5	S	0.507	0.492	2.9
30 2-Fluorobiphenyl	S	0.849	0.864	-1.7
31 2,4,6-Tribromophenol	S	0.134	0.111	17.2
32 Phenol-d5	S	1.617	1.589	1.8
33 Pyrene-d10	S	0.771	0.871	-13.1
34 Anthracene-d10	S	0.892	0.880	1.3
35 1,4-Dibromobenzene-d4	S	0.693	0.619	10.8
36 1,3,5-Trichlorobenzene-d3	S	0.269	0.256	4.9

25-Sep-91 11:36
Sample: SSTD020

Triangle Labs, Inc.

201

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Instrument F



No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM	Name
1	100	85	100	-1	133290	bb	301	152	1,4 Dichlorobenzene-d4
2	100	87	91	1	499180	bb	477	136	Naphthalene-d8
3	100	93	96	-1	258510	bb	479	128	Naphthalene
4	99	71	88	0	202750	bb	581	142	2-Methylnaphthalene
5	100	94	96	0	343080	bb	728	164	Acenaphthene-d10
6	100	92	95	0	161280	bb	649	162	2-Chloronaphthalene
7	100	95	98	-1	270950	bb	705	152	Acenaphthylene
8	100	88	98	-1	179790	bb	732	153	Acenaphthene
9	100	93	95	-1	209040	bb	807	166	Fluorene
10	100	93	97	0	781260	vv	940	188	Phenanthrene-d10
11	100	95	98	-2	363540	vv*	942	178	Phenanthrene
12	100	94	97	-1	362460	vb	950	178	Anthracene
13	100	96	98	-2	590440	bb	1113	202	Fluoranthene
14	89	73	93	-2	1163500	bv	1326	240	Chrysene-d12
15	100	94	98	1	452760	bb	1185	244	Terphenyl-d14
16	100	95	97	0	611140	bb	1143	202	Pyrene
17	100	81	97	0	590610	bv*	1324	228	Benzo(a)anthracene
18	100	94	99	0	627860	vb	1329	228	Chrysene
19	100	88	92	1	1071800	bb	1540	264	Perylene-d12
20	100	89	93	-2	532110	bv	1485	252	Benzo(b)fluoranthene
21	100	93	95	-2	623110	vb	1490	252	Benzo(k)fluoranthene
22	100	93	99	-1	510600	bv	1523	252	Benzo(e)pyrene
23	100	94	100	-2	513150	vv	1530	252	Benzo(a)pyrene
24	100	82	99	-1	353140	vb	1543	252	Perylene
25	97	90	90	-2	283810	bv	1681	276	Indeno(1,2,3-cd)pyrene
26	100	86	87	-1	344260	bv	1690	278	Dibenz(a,h)anthracene
27	98	89	93	-2	399360	vb	1712	276	Benzo(g,h,i)perylene
28	76	57	64	0	24712	bb	919	266	Pentachlorophenol
29	87	58	91	-1	131750	bb	380	82	Nitrobenzene-d5
30	100	95	97	-1	158960	bb	642	172	2-Fluorobiphenyl
31	84	68	76	-1	21848	bb	843	330	2,4,6-Tribromophenol
32	98	73	95	-1	101960	bb	271	99	Phenol-d5
33	100	91	97	0	458140	bb	1140	212	Pyrene-d10
34	100	91	97	-2	372680	vb	947	188	Anthracene-d10
35	100	92	95	1	52172	bb	485	240	1,4-Dibromobenzene-d4
36	95	69	83	0	72372	bb	427	185	1,3,5-Trichlorobenzene-

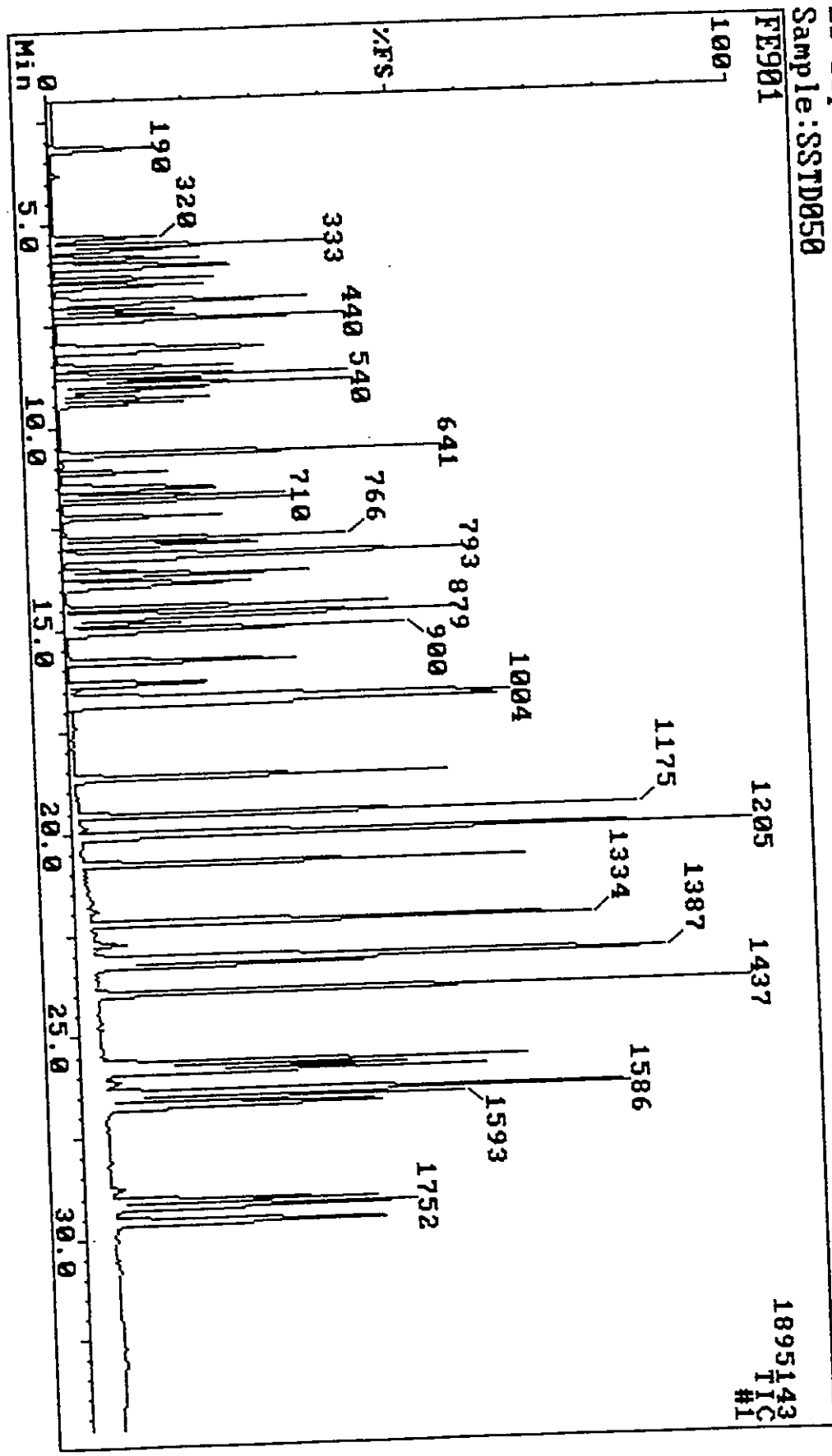
25-Sep-91 08:33

Sample: SSTD050

FE901

Triangle Labs, Inc.

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Instrument F



1895143
TIC
#1

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	82	99	0	153760	bb	362	152 1,4 Dichlorobenzene-d4
2	100	89	95	0	589980	bb	537	136 Naphthalene-d8
3	100	91	95	1	693840	bb	540	128 Naphthalene
4	58	72	90	5	585700	bb	641	142 2-Methylnaphthalene
5	100	93	98	0	384900	bb	788	164 Acenaphthene-d10
6	100	94	97	-2	444400	bb	709	162 2-Chloronaphthalene
7	100	94	97	-1	740720	bb	766	152 Acenaphthylene
8	100	87	97	1	470470	bb	793	153 Acenaphthene
9	93	93	96	3	549220	bb	868	166 Fluorene
10	100	91	97	0	896170	bv	1000	188 Phenanthrene-d10
11	100	93	97	1	970800	vv*	1004	178 Phenanthrene
12	100	91	97	0	977240	vb*	1011	178 Anthracene
13	86	94	97	4	1456600	vv	1175	202 Fluoranthene
14	100	71	93	0	1004200	bb	1388	240 Chrysene-d12
15	100	89	98	0	1026700	bb	1246	244 Terphenyl-d14
16	100	93	97	-1	1458600	bb	1205	202 Pyrene
17	100	85	97	0	1379800	bv	1386	228 Benzo(a)anthracene
18	100	90	98	-1	1277600	vb	1391	228 Chrysene
19	100	80	93	0	874530	bb	1601	264 Perylene-d12
20	100	87	95	0	1064700	bv	1548	252 Benzo(b)fluoranthene
21	100	89	96	0	1303900	vv	1553	252 Benzo(k)fluoranthene
22	99	60	99	0	1065700	bv*	1585	252 Benzo(e)pyrene
23	100	86	100	0	1118100	vv	1593	252 Benzo(a)pyrene
24	100	84	99	0	634220	vv	1605	252 Perylene
25	100	88	95	1	885200	bv	1744	276 Indeno(1,2,3-cd)pyrene
26	100	84	93	1	921530	vv	1752	278 Dibenz(a,h)anthracene
27	100	86	95	1	1007200	vv	1775	276 Benzo(g,h,i)perylene
28	100	84	96	0	135020	bb	979	266 Pentachlorophenol
29	71	51	93	-3	363100	bb	441	82 Nitrobenzene-d5
30	100	91	97	-1	415810	bb	703	172 2-Fluorobiphenyl
31	68	77	91	5	53308	bb	904	330 2,4,6-Tribromophenol
32	89	60	94	0	305140	bb	333	99 Phenol-d5
33	100	82	98	-1	1093900	bb	1202	212 Pyrene-d10
34	100	86	97	1	986240	vb	1009	188 Anthracene-d10
35	100	82	94	-1	118890	bb	546	240 1,4-Dibromobenzene-d4
36	91	71	85	-1	188430	bb	487	185 1,3,5-Trichlorobenzene-

25-Sep-91 10:51

Sample: SSTD080

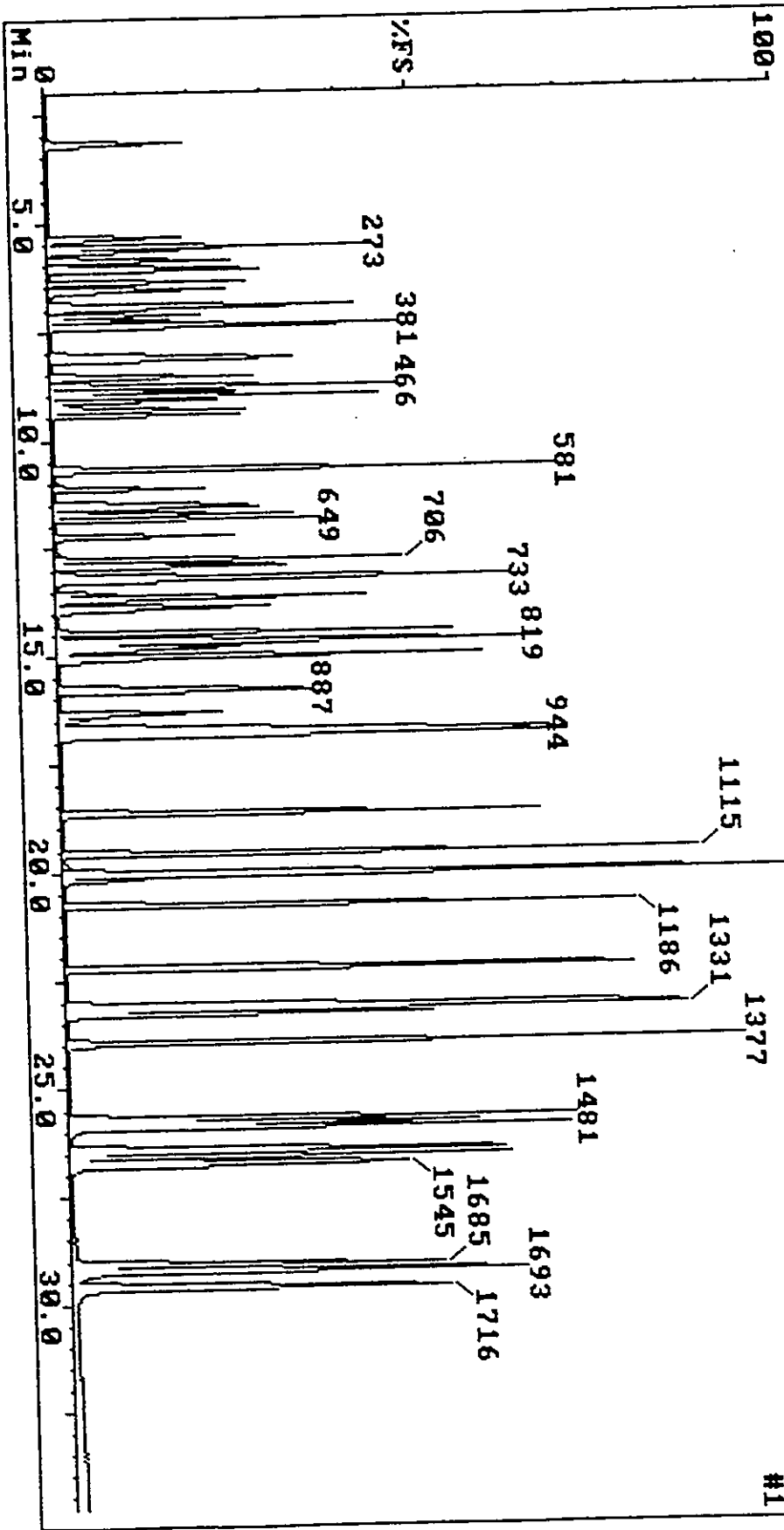
Triangle Labs, Inc.

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Instrument F

FE904

2045972
TIC
#1

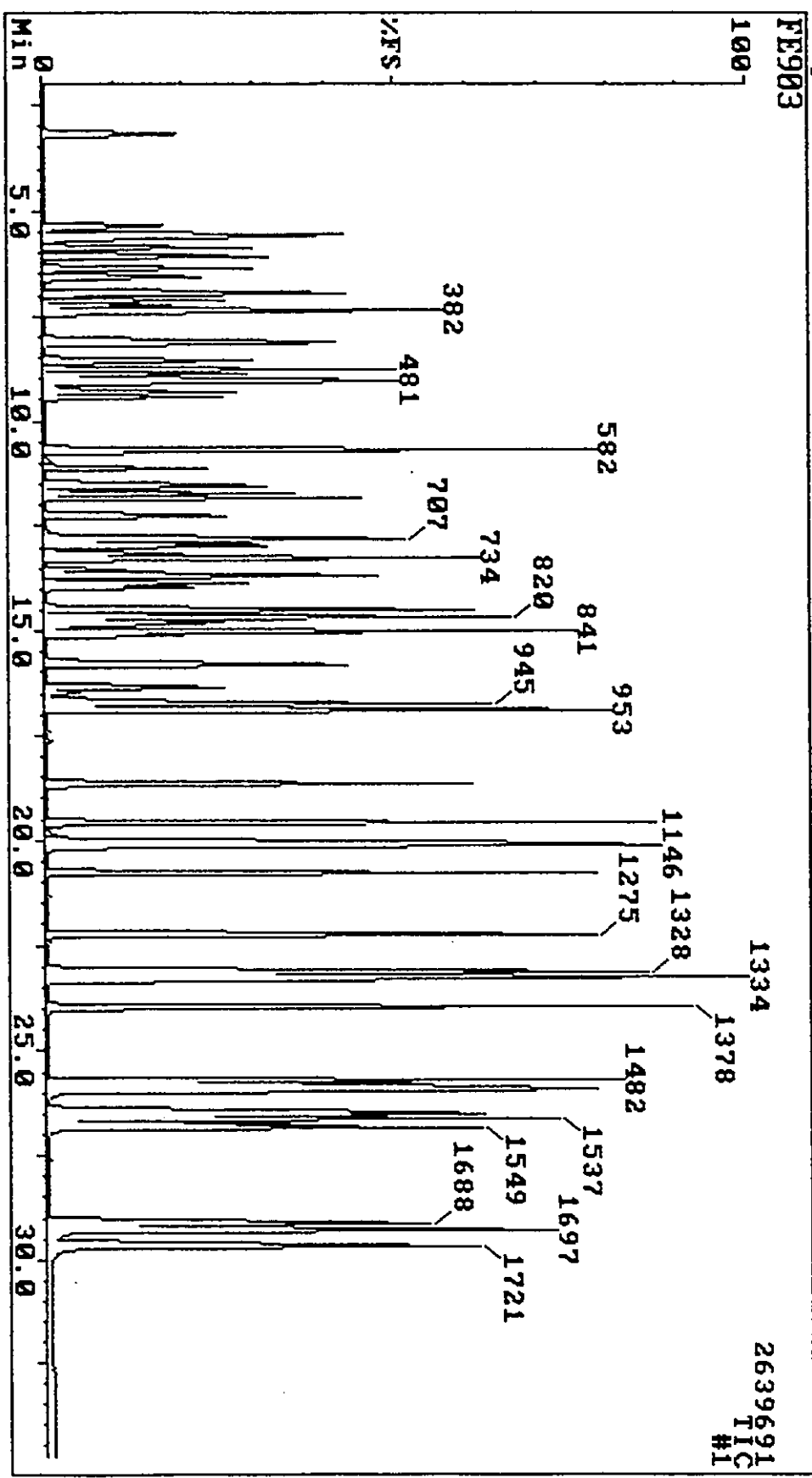


Io.	MAT	FDR	REV	Delta	Area	F.Flags	Scan	QM Name
1	100	79	100	-1	111230	bb	301	152 1,4 Dichlorobenzene-d4
2	100	82	92	1	415410	bb	477	136 Naphthalene-d8
3	100	92	95	0	810870	bb	480	128 Naphthalene
4	95	65	87	0	666200	bb	581	142 2-Methylnaphthalene
5	100	89	97	0	281680	bb	728	164 Acenaphthene-d10
6	100	93	96	0	515200	bb	649	162 2-Chloronaphthalene
7	100	93	97	0	871840	bb	706	152 Acenaphthylene
8	100	84	97	0	576910	bb	733	153 Acenaphthene
9	100	93	97	0	645700	bb	808	166 Fluorene
10	100	90	96	0	696750	vv	940	188 Phenanthrene-d10
11	100	93	97	0	1229600	vv*	944	178 Phenanthrene
12	100	93	98	0	1195500	vb*	951	178 Anthracene
13	100	95	98	0	1845100	vv	1115	202 Fluoranthene
14	84	51	94	-1	864770	bv	1327	240 Chrysene-d12
15	100	90	98	1	1367600	bb	1186	244 Terphenyl-d14
16	100	95	97	1	1748100	bb	1145	202 Pyrene
17	100	91	97	0	1812300	bv*	1325	228 Benzo(a)anthracene
18	100	93	98	1	1774700	vb	1331	228 Chrysene
19	100	86	92	1	873250	bb	1541	264 Perylene-d12
20	100	92	95	0	1795800	bv	1488	252 Benzo(b)fluoranthene
21	100	93	96	0	1759000	vv	1493	252 Benzo(k)fluoranthene
22	100	93	99	1	1652800	bv*	1526	252 Benzo(e)pyrene
23	100	93	100	0	1706900	vv*	1533	252 Benzo(a)pyrene
24	100	92	99	0	990800	vv	1545	252 Perylene
25	100	94	96	1	1528300	bv	1685	276 Indeno(1,2,3-cd)pyrene
26	100	91	95	1	1645500	vv	1693	278 Dibenz(a,h)anthracene
27	100	92	94	1	1698700	b? <i>not m</i>	1716	276 Benzo(g,h,i)perylene
28	100	83	95	0	180300	bv	919	266 Pentachlorophenol
29	89	60	94	0	447490	bb	381	82 Nitrobenzene-d5
30	100	89	96	0	484710	bb	643	172 2-Fluorobiphenyl
31	100	79	92	0	91384	bb	844	330 2,4,6-Tribromophenol
32	81	51	89	1	385040	bb	273	99 Phenol-d5
33	100	78	96	1	1401000	bb	1142	212 Pyrene-d10
34	100	84	97	0	1238400	vb	949	188 Anthracene-d10
35	100	89	96	1	172560	bb	485	240 1,4-Dibromobenzene-d4
36	95	67	85	0	233830	bb	427	185 1,3,5-Trichlorobenzene-

25-Sep-91 10:06
Sample: SSTD120

Triangle Labs, Inc.

(919) 544-5729
Instrument F



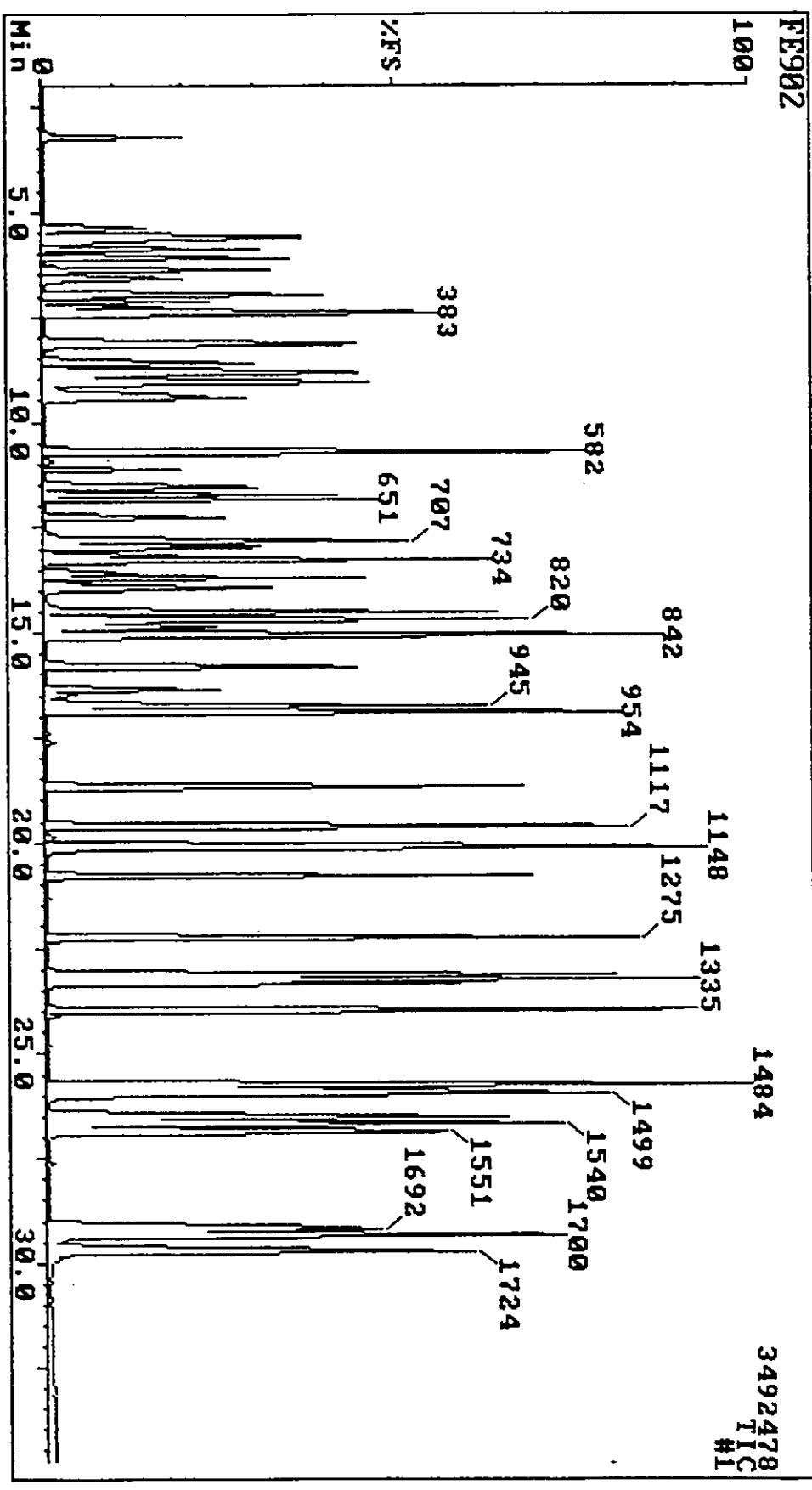
2639691
TIC
#1

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	61	99	0	113460	bb	302	152 1,4 Dichlorobenzene-d4
2	94	69	92	1	420650	bb	478	136 Naphthalene-d8
3	100	92	95	0	1248000	bb	481	128 Naphthalene
4	98	68	88	0	1024900	bb	582	142 2-Methylnaphthalene
5	100	87	97	-1	289100	bb	728	164 Acenaphthene-d10
6	100	92	96	1	781230	bb	650	162 2-Chloronaphthalene
7	100	93	97	1	1356300	bb	707	152 Acenaphthylene
8	100	90	98	1	869320	bb	734	153 Acenaphthene
9	100	92	96	1	976460	bb	809	166 Fluorene
10	100	87	96	0	646990	vv	940	188 Phenanthrene-d10
11	100	94	98	1	1705600	vv	945	178 Phenanthrene
12	100	93	98	2	1732600	vb	953	178 Anthracene
13	100	95	98	1	2623400	vv	1116	202 Fluoranthene
14	88	59	93	1	953500	bb	1329	240 Chrysene-d12
15	100	90	98	0	1928200	bb	1187	244 Terphenyl-d14
16	100	94	97	0	2447200	bb	1146	202 Pyrene
17	100	91	97	0	3106800	bv*	1327	228 Benzo(a)anthracene
18	100	92	99	2	2818200	vb	1334	228 Chrysene
19	94	83	92	2	1072400	bb	1544	264 Perylene-d12
20	100	92	95	0	3636400	b! ✓	1491	252 Benzo(b)fluoranthene
21	100	93	96	0	2969800	!b ✓	1496	252 Benzo(k)fluoranthene
22	100	93	99	1	3113500	bv	1529	252 Benzo(e)pyrene
23	100	92	100	1	3188800	vv	1537	252 Benzo(a)pyrene
24	100	92	99	1	1827400	vv	1549	252 Perylene
25	100	93	96	1	3061500	bv	1688	276 Indeno(1,2,3-cd)pyrene
26	99	90	95	2	3169500	vv	1697	278 Dibenz(a,h)anthracene
27	92	92	94	3	3136300	b? ✓	1721	276 Benzo(g,h,i)perylene
28	100	83	97	1	266080	bb	920	266 Pentachlorophenol
29	87	56	94	0	676840	bb	382	82 Nitrobenzene-d5
30	100	91	97	0	715050	bb	643	172 2-Fluorobiphenyl
31	99	79	92	1	133520	bb	845	330 2,4,6-Tribromophenol
32	81	50	89	1	587120	bb	274	99 Phenol-d5
33	100	83	98	0	2005700	bb	1143	212 Pyrene-d10
34	100	80	97	1	1746700	vb	950	188 Anthracene-d10
35	100	87	95	0	243420	bb	486	240 1,4-Dibromobenzene-d4
36	89	58	85	0	347460	bb	428	185 1,3,5-Trichlorobenzene-

25-Sep-91 09:30
Sample: SSTD160

Triangle Labs, Inc. *and*

(919) 544-5729
Instrument F



o.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	61	99	0	135480	bb	302	152 1,4 Dichlorobenzene-d4
2	95	69	94	1	504960	bb	478	136 Naphthalene-d8
3	100	93	96	0	1949400	bb	481	128 Naphthalene
4	99	69	90	0	1732600	bv	582	142 2-Methylnaphthalene
5	100	82	97	0	345920	vb	729	164 Acenaphthene-d10
6	100	93	96	1	1184000	bb	651	162 2-Chloronaphthalene
7	100	94	98	0	2147100	bb	707	152 Acenaphthylene
8	100	90	98	0	1352700	bb	734	153 Acenaphthene
9	100	92	96	1	1523100	bb	810	166 Fluorene
10	100	80	96	0	751810	vv	941	188 Phenanthrene-d10
11	100	94	98	0	2516600	vv	945	178 Phenanthrene
12	100	94	98	2	2496100	vb	954	178 Anthracene
13	100	95	98	1	3680800	vv	1117	202 Fluoranthene
14	81	46	94	1	1026400	bb	1330	240 Chrysene-d12
15	100	90	98	-1	2589000	bb	1187	244 Terphenyl-d14
16	100	94	97	1	3672800	bb	1148	202 Pyrene
17	100	91	97	0	4357600	bv*	1328	228 Benzo(a)anthracene
18	100	93	99	2	3864800	vb	1335	228 Chrysene
19	86	82	93	3	1224200	bb	1546	264 Perylene-d12
20	100	92	95	1	5998900	b!* <i>1-15-91</i>	1494	252 Benzo(b)fluoranthene
21	100	93	96	1	3466300	!b	1499	252 Benzo(k)fluoranthene
22	100	93	99	2	4795300	bv	1532	252 Benzo(e)pyrene
23	100	92	100	2	4462300	vv	1540	252 Benzo(a)pyrene
24	100	92	99	1	2726000	vv	1551	252 Perylene
25	94	94	97	3	4571700	bv	1692	276 Indeno(1,2,3-cd)pyrene
26	91	90	95	3	4763800	bv	1700	278 Dibenz(a,h)anthracene
27	92	92	95	3	4430500	bv	1724	276 Benzo(g,h,i)perylene
28	100	83	97	0	358600	bv	920	266 Pentachlorophenol
29	78	50	95	1	887560	bb	383	82 Nitrobenzene-d5
30	100	90	97	0	1067600	bb	644	172 2-Fluorobiphenyl
31	99	78	92	1	158400	bb	846	330 2,4,6-Tribromophenol
32	75	51	89	2	819940	bb	275	99 Phenol-d5
33	100	76	96	0	2803000	bb	1144	212 Pyrene-d10
34	100	77	97	1	2516900	vb	951	188 Anthracene-d10
35	100	86	96	0	311280	bb	486	240 1,4-Dibromobenzene-d4
36	88	55	85	0	486660	bb	428	185 1,3,5-Trichlorobenzene-

25-Sep-91 07:56

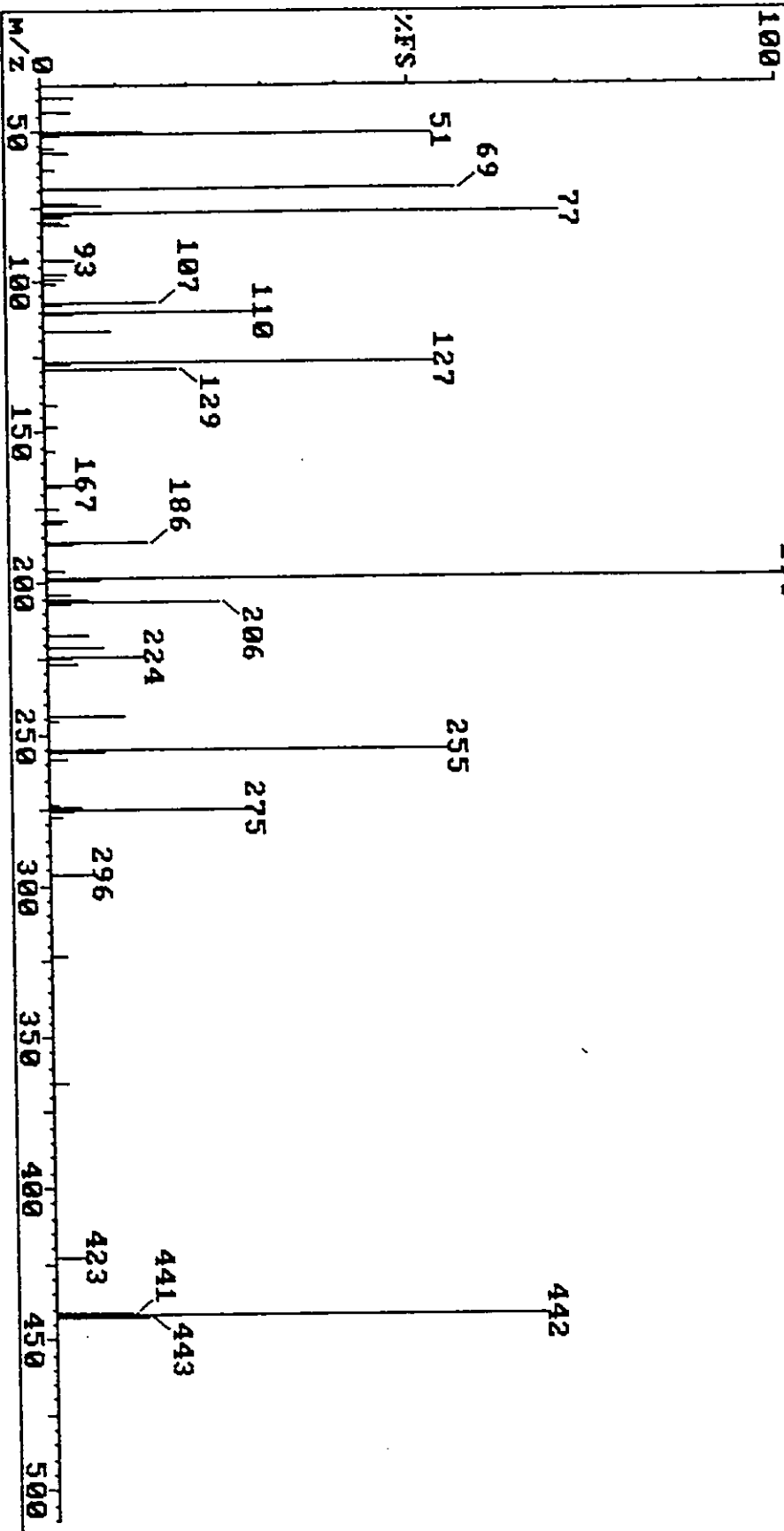
Triangle Labs, Inc.

Sample: DFTPP

(919) 544-5729
Instrument F

FE900 372 (5.100)

39168



FE900 372 (5.100)

PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int
1	39	1696	4.33	15	80	896	2.29	29	141	616	1.57	43	285	2160	5.51	57	274	1664	4.25
2	44	1536	3.92	16	81	1328	3.39	30	148	628	1.60	44	286	9088	23.20	58	275	10304	26.31
3	50	5376	13.73	17	93	1696	4.33	31	156	516	1.32	45	287	1184	3.02	59	276	1264	3.23
4	51	28736	52.94	18	98	1232	3.15	32	167	1600	4.08	46	217	2128	5.43	60	277	668	1.71
5	52	944	2.41	19	99	1856	2.78	33	168	768	1.96	47	221	2864	7.31	61	296	2112	5.39
6	56	548	1.40	20	101	636	1.62	34	175	568	1.45	48	224	4992	12.75	62	323	708	1.81
7	57	1360	3.47	21	107	6816	15.36	35	179	1072	2.74	49	225	1152	2.94	63	365	736	1.86
8	63	572	1.46	22	108	864	2.21	36	180	828	2.11	50	227	1520	3.88	64	423	1472	3.76
9	69	22816	56.21	23	110	11072	28.27	37	186	5376	13.73	51	244	3904	9.97	65	441	4000	10.21
10	74	1840	4.70	24	111	1456	3.72	38	187	1440	3.68	52	246	584	1.29	66	442	26112	66.67
11	75	2976	7.60	25	117	3520	8.99	39	196	888	2.27	53	255	21248	54.25	67	443	4928	12.56
12	77	27392	69.93	26	127	28736	52.94	40	198	39168	100.00	54	256	2944	7.52				
13	78	1600	4.08	27	128	1424	3.64	41	199	2768	7.07	55	258	928	2.37				
14	79	1128	2.86	28	129	6976	17.81	42	204	1200	3.06	56	273	528	1.35				

DFTFP TUNE CHECK REPORT

Raw Data File: FE900
 Date: 25-Sep-91
 Time: 07:56

M/E	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	52.94	PASS
68	Less than 2.0% of mass 69	0.00(0.0)1	PASS
69	Mass 69 relative abundance	56.21	PASS
70	Less than 2.0% of mass 69	0.00(0.0)1	PASS
127	40.0 - 60.0% of mass 198	52.94	PASS
197	Less than 1% of mass 198	0.00	PASS
198	Base peak, 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	7.07	PASS
275	10 - 30% of mass 198	26.31	PASS
365	Greater than 1% of mass 198	1.88	PASS
441	Present, but less than mass 443	10.21	PASS
442	Greater than 40% of mass 198	66.67	PASS
443	17 - 23% of mass 442	12.58(18.9)2	PASS

ms
INITIAL CALIBRATION CHECK

DATE : 19-Se

NB
9-20-91

TIME : 1

LAB FILE ID: RF20 =FE812 RF50 =FE807 RF80 =FE811
 RF120=FE810 RF160=FE809

COMPOUND	FLAG	RF 20NG	RF 50NG	RF 80NG	RF 120NG	RF 160NG	RF MEAN	%RSI
3 Naphthalene		0.938	0.910	0.933	0.945	0.934	0.932	1.0
4 2-Methylnaphthalene		0.558	0.719	0.609	0.547	0.768	0.640	15.0
6 2-Chloronaphthalene		0.954	0.933	0.963	0.966	0.947	0.952	1.0
7 Acenaphthylene		1.505	1.512	1.545	1.614	1.564	1.548	2.0
8 Acenaphthene	C	1.036	1.007	1.034	1.073	1.042	1.038	2.0
9 Fluorene		0.922	0.941	0.980	1.045	1.091	0.996	7.0
11 Phenanthrene		1.056	1.077	1.010	0.946	0.894	0.997	7.0
12 Anthracene		1.068	1.018	0.999	0.888	0.838	0.962	9.0
13 Fluoranthene	C	1.085	1.170	1.192	1.020	0.980	1.089	8.0
16 Pyrene		0.853	0.938	0.909	0.925	0.892	0.903	3.0
17 Benzo(a)anthracene		0.990	1.023	1.049	1.080	1.049	1.038	3.0
18 Chrysene		1.023	1.040	1.064	1.043	0.967	1.027	3.0
20 Benzo(b)fluoranthene		0.871	0.883	0.872	0.916	0.967	0.902	4.0
21 Benzo(k)fluoranthene		1.064	0.978	1.040	0.983	0.900	0.993	6.0
22 Benzo(e)pyrene		0.856	0.849	0.915	0.933	0.922	0.895	4.0
23 Benzo(a)pyrene	C	0.912	0.945	0.976	0.999	0.930	0.952	3.0
24 Perylene		0.643	0.563	0.586	0.570	0.550	0.582	6.0
25 Indeno(1,2,3-cd)pyrene		0.634	0.860	0.903	0.939	0.942	0.855	15.0
26 Dibenz(a,h)anthracene		0.772	0.923	0.981	1.066	1.017	0.952	11.0
27 Benzo(g,h,i)perylene		0.927	0.962	1.037	1.080	0.995	1.000	6.0
28 Pentachlorophenol	C	0.079	0.090	0.093	0.081	0.073	0.083	9.0
=====								
15 Terphenyl-d14	S	0.565	0.629	0.611	0.649	0.602	0.611	5.0
29 Nitrobenzene-d5	S	0.297	0.254	0.269	0.283	0.280	0.277	5.0
30 2-Fluorobiphenyl	S	0.876	0.896	0.907	0.908	0.858	0.889	2.0
31 2,4,6-Tribromophenol	S	0.074	0.078	0.081	0.093	0.094	0.084	10.0
32 Phenol-d5	S	1.460	1.196	1.314	1.337	1.402	1.342	7.0
33 Pyrene-d10	S	0.590	0.655	0.619	0.677	0.649	0.638	5.0
34 Anthracene-d10	S	0.942	0.924	0.891	0.748	0.734	0.848	11.0
35 1,4-Dibromobenzene-d4	S	0.413	0.470	0.478	0.477	0.486	0.465	6.0
36 1,3,5-Trichlorobenzene-d3	S	0.197	0.207	0.212	0.213	0.203	0.206	3.0

ms
DAILY CALIBRATION CHECK

DATE : 19-Sep

TIME : 17

LAB FILE ID: FE807

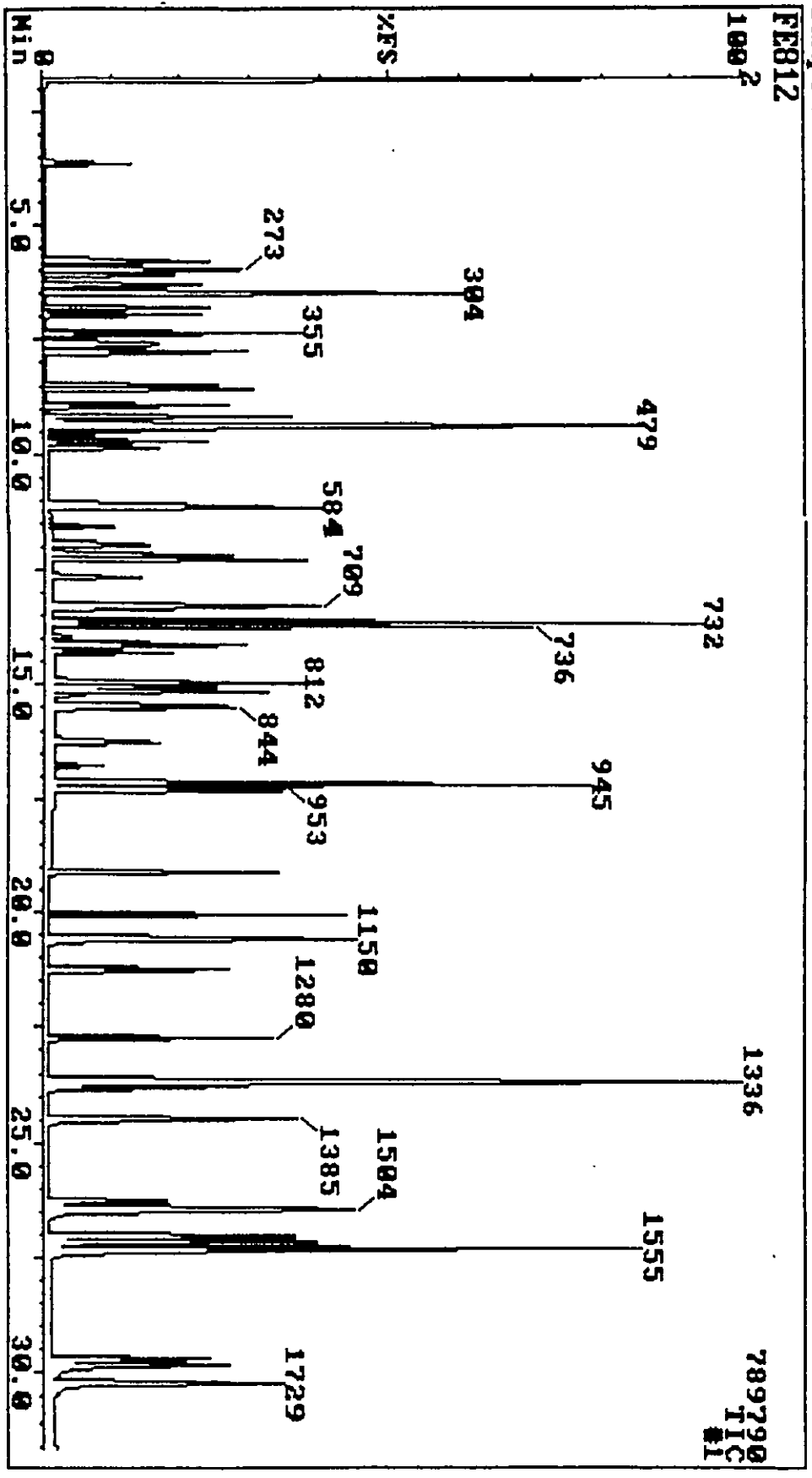
NB
9-20-91

COMPOUND	FLAG	RF MEAN	RF 50	%D
3 Naphthalene		0.932	0.910	2.3
4 2-Methylnaphthalene		0.640	0.719	-12.3
6 2-Chloronaphthalene		0.952	0.933	2.1
7 Acenaphthylene		1.548	1.512	2.3
8 Acenaphthene	C	1.038	1.007	3.0
9 Fluorene		0.996	0.941	5.5
11 Phenanthrene		0.997	1.077	-8.1
12 Anthracene		0.962	1.018	-5.8
13 Fluoranthene	C	1.089	1.170	-7.4
16 Pyrene		0.903	0.938	-3.8
17 Benzo(a)anthracene		1.038	1.023	1.4
18 Chrysene		1.027	1.040	-1.2
20 Benzo(b)fluoranthene		0.902	0.883	2.1
21 Benzo(k)fluoranthene		0.993	0.978	1.5
22 Benzo(e)pyrene		0.895	0.849	5.2
23 Benzo(a)pyrene	C	0.952	0.945	0.8
24 Perylene		0.582	0.563	3.3
25 Indeno(1,2,3-cd)pyrene		0.855	0.860	-0.5
26 Dibenz(a,h)anthracene		0.952	0.923	3.1
27 Benzo(g,h,i)perylene		1.000	0.962	3.8
28 Pentachlorophenol	C	0.083	0.090	-8.4
=====				
15 Terphenyl-d14	S	0.611	0.629	-2.9
29 Nitrobenzene-d5	S	0.277	0.254	8.1
30 2-Fluorobiphenyl	S	0.889	0.896	-0.8
31 2,4,6-Tribromophenol	S	0.084	0.078	7.4
32 Phenol-d5	S	1.342	1.196	10.9
33 Pyrene-d10	S	0.638	0.655	-2.7
34 Anthracene-d10	S	0.848	0.924	-9.0
35 1,4-Dibromobenzene-d4	S	0.465	0.470	-1.1
36 1,3,5-Trichlorobenzene-d3	S	0.206	0.207	-0.2

19-Sep-91 16:19
Sample: SSTW020

Triangle Labs, Inc.

(919) 544-5729
Instrument F

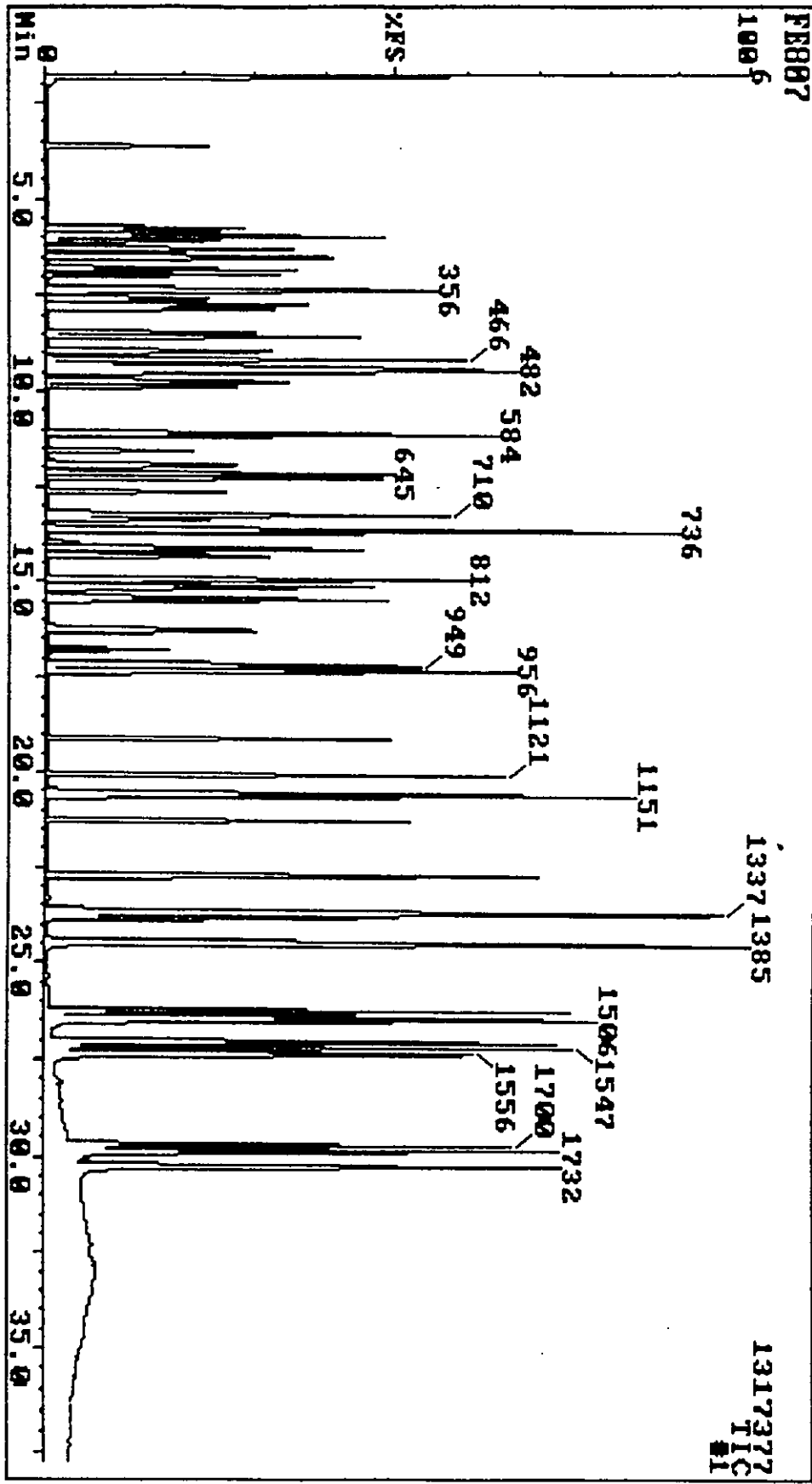


No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM	Name
1	100	85	99	0	173730	bb	304	152	1,4 Dichlorobenzene-d4
2	100	93	96	-1	706000	bb	479	136	Naphthalene-d8
3	100	96	98	1	331010	bb	482	128	Naphthalene
4	100	92	97	1	196830	vb	584	142	2-Methylnaphthalene
5	100	96	98	1	365780	bb	732	164	Acenaphthene-d10
6	100	95	98	0	174400	bb	652	162	2-Chloronaphthalene
7	100	96	99	-1	275300	bb	709	152	Acenaphthylene
8	100	77	98	0	189380	bb	736	153	Acenaphthene
9	100	90	94	0	168680	bb	812	166	Fluorene
10	100	92	96	0	401890	bv	945	188	Phenanthrene-d10
11	100	94	98	0	212140	bv	948	178	Phenanthrene
12	100	94	99	-1	214540	vb*	955	178	Anthracene
13	100	94	96	-1	218050	bb	1120	202	Fluoranthene
14	100	81	92	-1	526970	bb	1336	240	Chrysene-d12
15	100	93	97	0	148910	bb	1191	244	Terphenyl-d14
16	100	93	95	0	224640	bb	1150	202	Pyrene
17	95	69	95	1	260820	bv	1335	228	Benzo(a)anthracene
18	100	94	100	0	269560	vb	1340	228	Chrysene
19	100	91	95	1	594540	bb	1555	264	Perylene-d12
20	95	87	90	-2	258970	bv	1499	252	Benzo(b)fluoranthene
21	99	91	93	-2	316250	vb	1504	252	Benzo(k)fluoranthene
22	100	93	98	-2	254480	bv*	1537	252	Benzo(e)pyrene
23	100	92	98	-2	271230	vv	1545	252	Benzo(a)pyrene
24	100	78	96	-1	191050	vb	1558	252	Perylene
25	97	90	90	-2	188530	bv	1698	276	Indeno(1,2,3-cd)pyrene
26	93	86	87	-2	229600	bv	1706	278	Dibenz(a,h)anthracene
27	89	88	92	-3	275440	vb	1729	276	Benzo(g,h,i)perylene
28	85	64	82	-1	15936	bb	922	266	Pentachlorophenol
29	100	91	95	1	104810	bb	382	82	Nitrobenzene-d5
30	100	93	97	-1	160170	bb	644	172	2-Fluorobiphenyl
31	76	53	68	-1	13608	bb	846	330	2,4,6-Tribromophenol
32	100	76	97	-1	126830	bv	272	99	Phenol-d5
33	100	93	97	0	155380	bb	1147	212	Pyrene-d10
34	100	89	97	0	189240	vb*	953	188	Anthracene-d10
35	100	93	94	-1	35856	bb	487	240	1,4-Dibromobenzene-d4
36	85	63	83	1	69536	bb	429	185	1,3,5-Trichlorobenzene-

19-Sep-91 12:17
Sample: SSTD050

Triangle Labs, Inc.

(919) 544-5729
Instrument F

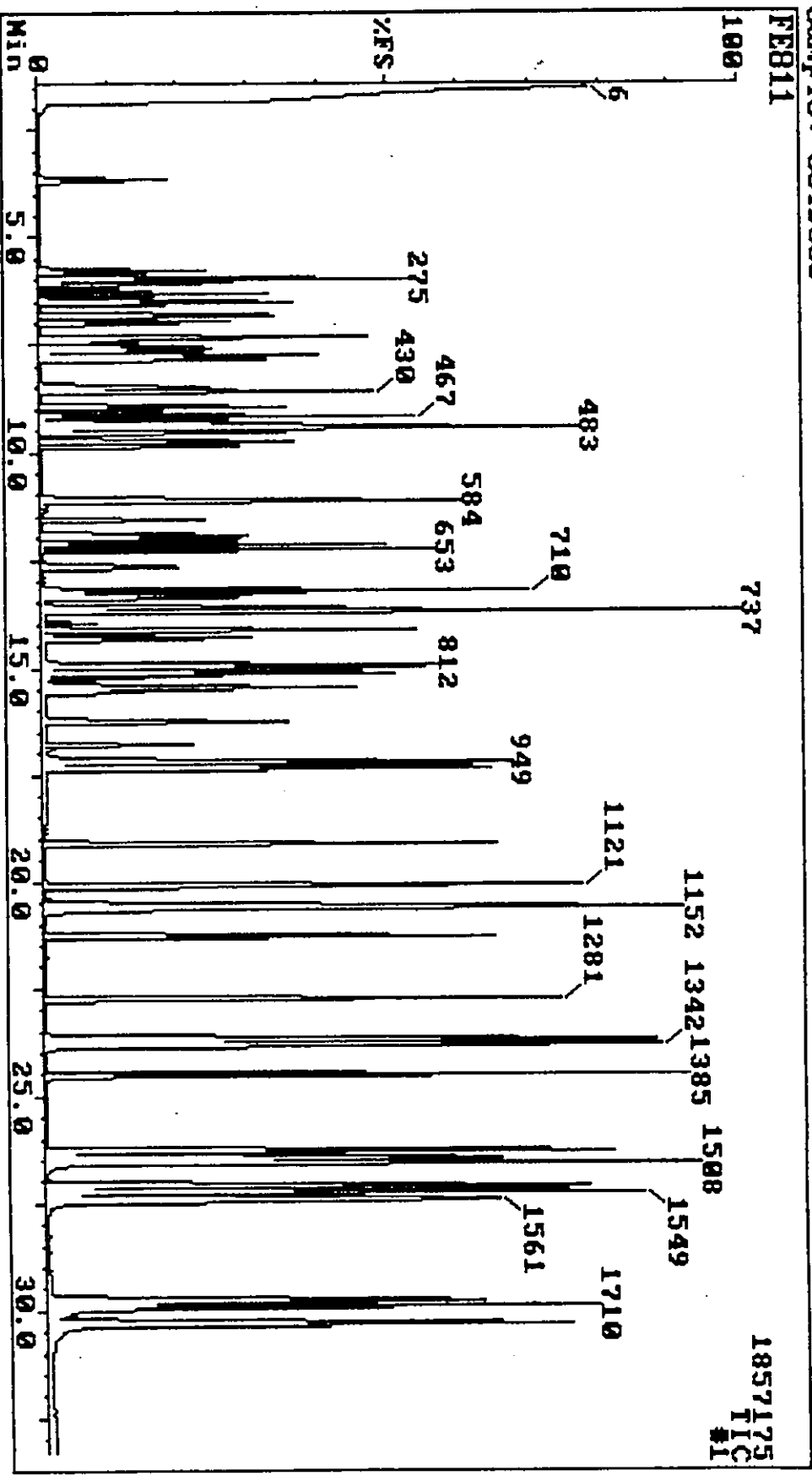


No.	MAT	FOR	REV	Delta	Area	F.Flags	Scan	QM	Name
1	100	82	98	0	194220	bb	304	152	1,4 Dichlorobenzene-d4
2	100	93	97	0	791950	bb	480	136	Naphthalene-d8
3	100	96	98	-2	901260	bb	482	128	Naphthalene
4	75	73	73	-9	711410	A	584	142	2-Methylnaphthalene
5	100	96	99	0	399470	bb	732	164	Acenaphthene-d10
6	100	97	98	8	465740	bb	652	162	2-Chloronaphthalene
7	100	96	99	2	755020	bb	710	152	Acenaphthylene
8	100	76	99	-2	502930	bb	736	153	Acenaphthene
9	94	96	98	-10	469630	bb	812	166	Fluorene
10	100	93	97	0	487620	vv*	945	188	Phenanthrene-d10
11	100	97	99	-2	656720	bv	948	178	Phenanthrene
12	100	96	98	-1	620220	vb	956	178	Anthracene
13	79	95	97	-15	713130	vb	1121	202	Fluoranthene
14	98	63	93	0	633900	bb	1337	240	Chrysene-d12
15	100	90	97	0	498240	bb	1192	244	Terphenyl-d14
16	96	95	97	9	743000	vb	1151	202	Pyrene
17	100	89	97	0	810910	bv	1335	228	Benzo(a)anthracene
18	100	94	99	1	823780	vb	1341	228	Chrysene
19	100	87	93	0	783720	bb	1555	264	Perylene-d12
20	100	91	94	2	865160	bv	1501	252	Benzo(b)fluoranthene
21	100	92	95	1	958390	vv	1506	252	Benzo(k)fluoranthene
22	100	92	98	0	831400	bv	1539	252	Benzo(e)pyrene
23	100	91	99	1	925600	vv	1547	252	Benzo(a)pyrene
24	100	89	98	0	551290	vv*	1559	252	Perylene
25	98	91	96	-7	842040	bv*	1700	276	Indeno(1,2,3-cd)pyrene
26	95	87	93	-7	903760	vv	1708	278	Dibenz(a,h)anthracene
27	94	89	95	-8	942420	bv	1732	276	Benzo(g,h,i)perylene
28	100	88	96	-3	54924	bb	923	266	Pentachlorophenol
29	75	92	95	16	251800	bb	382	82	Nitrobenzene-d5
30	100	95	99	5	447200	bb	645	172	2-Fluorobiphenyl
31	66	76	83	-15	38900	bb	847	330	2,4,6-Tribromophenol
32	100	79	97	-3	290350	bb	273	99	Phenol-d5
33	95	90	96	8	518770	bb	1148	212	Pyrene-d10
34	100	92	98	0	563310	vb*	953	188	Anthracene-d10
35	100	89	94	0	114050	bb	488	240	1,4-Dibromobenzene-d4
36	80	70	86	8	204720	bb	429	185	1,3,5-Trichlorobenzene-d

19-Sep-91 15:24
Sample: SST00880

Triangle Labs, Inc.

(919) 544-5729
Instrument F

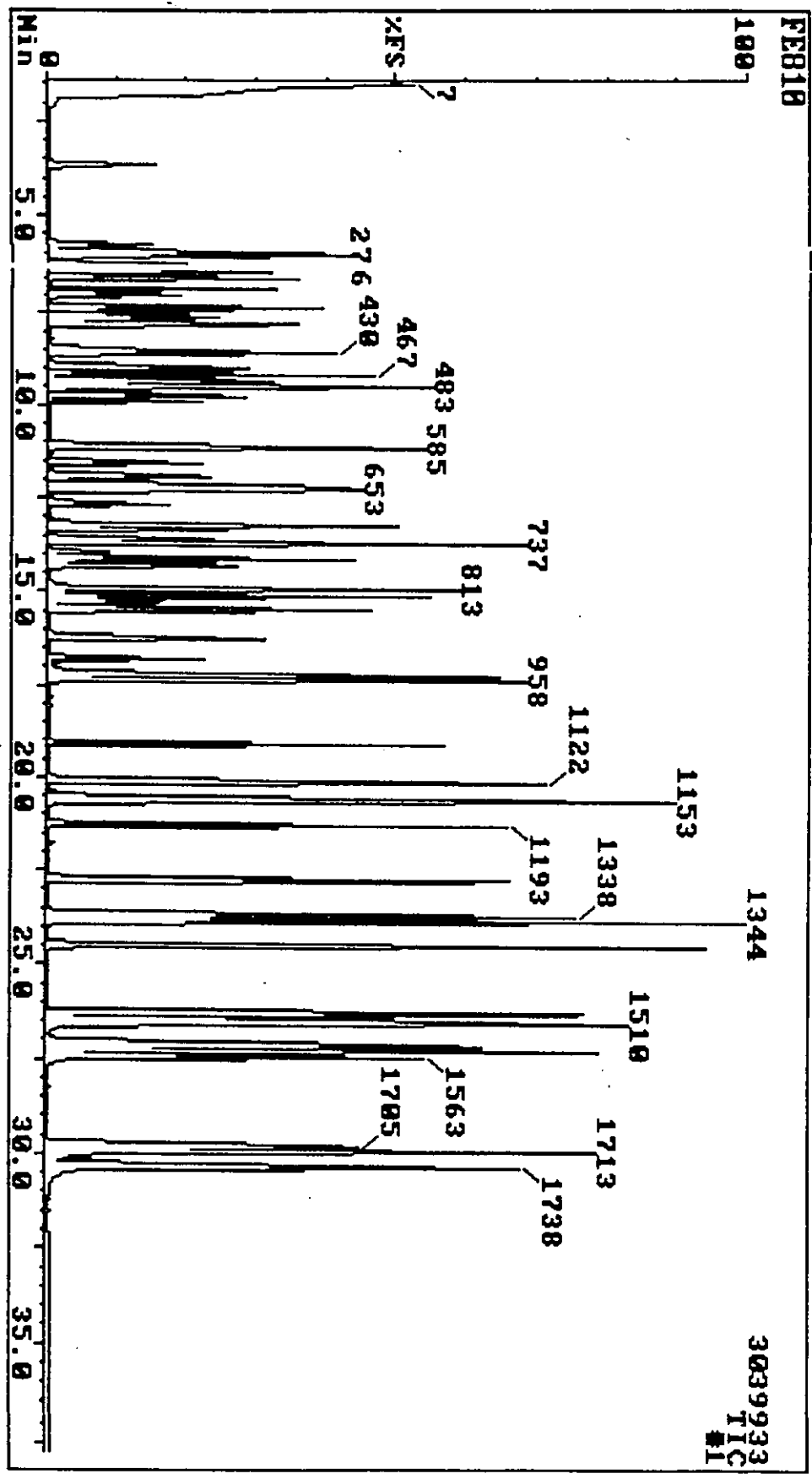


No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	80	98	0	178800	bb	304	152 1,4 Dichlorobenzene-d4
2	100	87	97	0	736790	bb	480	136 Naphthalene-d8
3	100	92	97	1	1375400	bb	483	128 Naphthalene
4	100	93	98	0	897540	vb	584	142 2-Methylnaphthalene
5	100	90	99	0	403140	bb	732	164 Acenaphthene-d10
6	100	95	98	1	776240	bb	653	162 2-Chloronaphthalene
7	100	95	99	0	1245700	bb	710	152 Acenaphthylene
8	100	78	99	1	833790	bb	737	153 Acenaphthene
9	100	93	96	0	789740	bb	812	166 Fluorene
10	100	88	96	0	494980	vv	945	188 Phenanthrene-d10
11	100	94	98	1	999550	vv	949	178 Phenanthrene
12	100	94	97	1	989160	vb*	957	178 Anthracene
13	100	95	97	0	1180400	vv	1121	202 Fluoranthene
14	89	59	94	1	703860	vb	1338	240 Chrysene-d12
15	100	90	98	-1	860060	vb	1192	244 Terphenyl-d14
16	100	93	96	0	1279300	vb	1152	202 Pyrene
17	100	91	97	0	1476500	vv*	1336	228 Benzo(a)anthracene
18	100	94	99	0	1497700	vb	1342	228 Chrysene
19	100	86	93	1	928090	bb	1557	264 Perylene-d12
20	100	92	95	-1	1618300	vv	1502	252 Benzo(b)fluoranthene
21	100	93	96	0	1930300	vb	1508	252 Benzo(k)fluoranthene
22	100	92	99	0	1698000	bv*	1541	252 Benzo(e)pyrene
23	100	92	99	0	1811600	vv	1549	252 Benzo(a)pyrene
24	100	90	98	0	1087200	vv	1561	252 Perylene
25	100	95	97	0	1676800	bv	1702	276 Indeno(1,2,3-cd)pyrene
26	100	90	94	0	1821600	vv	1710	278 Dibenz(a,h)anthracene
27	100	93	95	1	1924800	b? <i>9.10.91</i>	1735	276 Benzo(g,h,i)perylene
28	100	83	96	0	91592	bb	923	266 Pentachlorophenol
29	100	86	98	1	396740	bb	383	82 Nitrobenzene-d5
30	100	94	99	0	731550	bb	645	172 2-Fluorobiphenyl
31	93	73	87	0	65024	bb	847	330 2,4,6-Tribromophenol
32	100	68	97	1	469840	bb	274	99 Phenol-d5
33	100	83	96	0	870960	vb	1149	212 Pyrene-d10
34	100	87	97	1	882130	vb	954	188 Anthracene-d10
35	100	79	96	0	170790	bb	488	240 1,4-Dibromobenzene-d4
36	98	71	86	0	312430	bb	429	185 1,3,5-Trichlorobenzene-

19-Sep-91 14:36
Sample: SSTD120

Triangle Labs, Inc.

(919) 544-5729
Instrument F

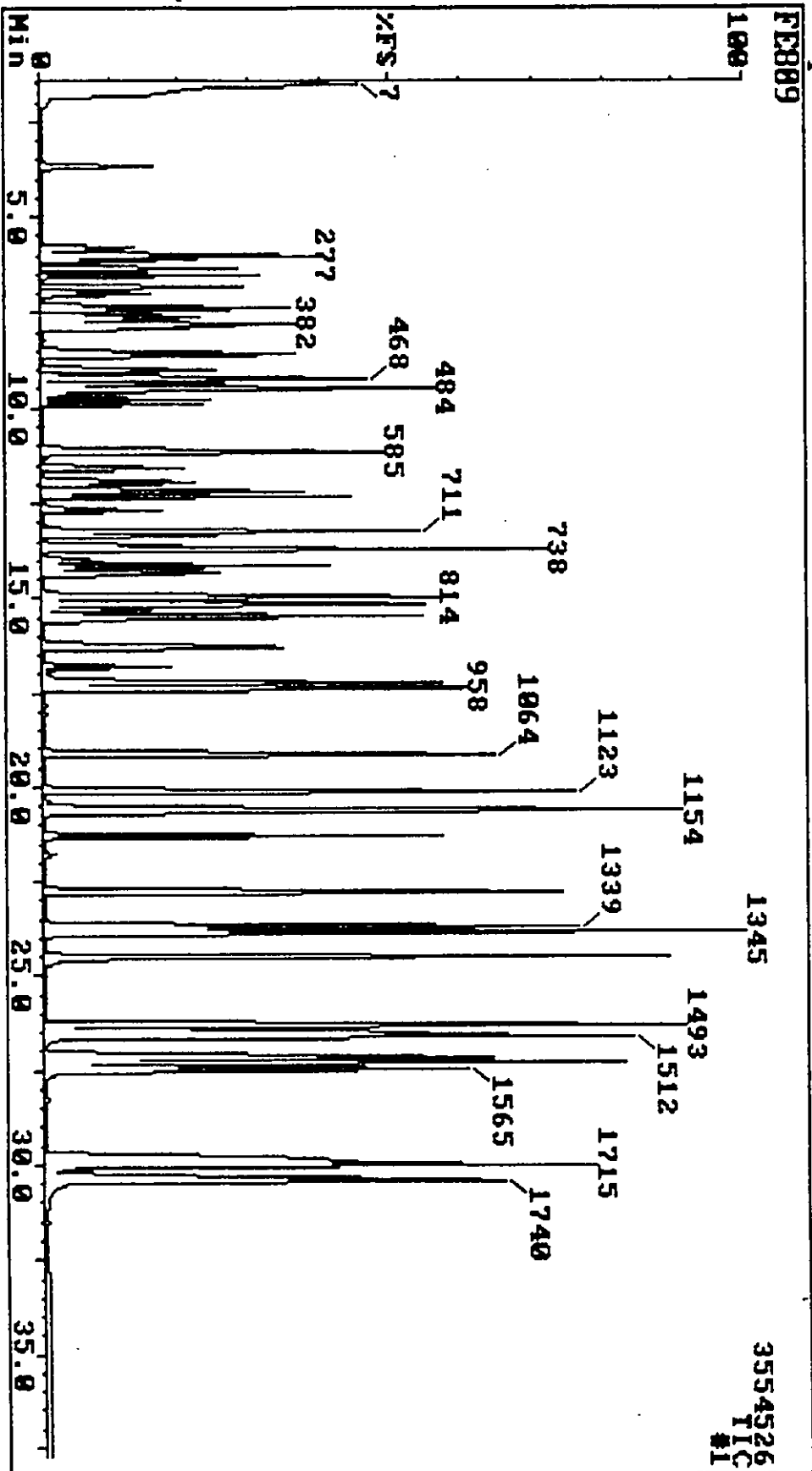


No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	76	98	0	173200	bb	304	152 1,4 Dichlorobenzene-d4
2	100	79	95	0	709380	bb	480	136 Naphthalene-d8
3	100	93	98	1	2012000	bb	483	128 Naphthalene
4	100	92	98	1	1163000	vb	585	142 2-Methylnaphthalene
5	100	81	99	0	400730	bb	732	164 Acenaphthene-d10
6	100	96	99	1	1161200	bb	653	162 2-Chloronaphthalene
7	100	95	99	0	1940800	bb	710	152 Acenaphthylene
8	100	81	99	1	1290100	bb	737	153 Acenaphthene
9	100	93	96	1	1255700	bb	813	166 Fluorene
10	100	81	96	1	688540	bv	946	188 Phenanthrene-d10
11	100	93	98	1	1954400	bv	950	178 Phenanthrene
12	100	94	98	1	1834000	vb	958	178 Anthracene
13	100	95	97	0	2106400	vv	1122	202 Fluoranthene
14	82	49	93	1	778130	bb	1339	240 Chrysene-d12
15	100	89	97	-1	1514900	bb	1193	244 Terphenyl-d14
16	100	93	97	0	2160000	vb	1153	202 Pyrene
17	100	92	97	1	2521200	vv*	1338	228 Benzo(a)anthracene
18	100	91	99	1	2433500	vb	1344	228 Chrysene
19	100	84	93	1	1034500	vb	1558	264 Perylene-d12
20	100	92	95	0	2842800	v!* <i>Low</i>	1504	252 Benzo(b)fluoranthene
21	100	93	96	1	3050000	vb	1510	252 Benzo(k)fluoranthene
22	100	92	99	2	2895400	vv	1544	252 Benzo(e)pyrene
23	100	92	99	2	3099200	vv	1552	252 Benzo(a)pyrene
24	100	91	98	1	1769500	vv	1563	252 Perylene
25	100	95	97	1	2912800	bv	1704	276 Indeno(1,2,3-cd)pyrene
26	99	90	94	2	3308000	bv	1713	278 Dibenz(a,h)anthracene
27	93	93	95	3	3352800	b? <i>Low</i>	1738	276 Benzo(g,h,i)perylene
28	100	83	97	0	167490	bb	924	266 Pentachlorophenol
29	93	75	98	2	601100	bb	384	82 Nitrobenzene-d5
30	100	93	98	1	1091000	bb	646	172 2-Fluorobiphenyl
31	90	71	84	1	112140	bb	848	330 2,4,6-Tribromophenol
32	88	58	94	2	694570	bb	275	99 Phenol-d5
33	100	77	97	0	1580200	vb	1150	212 Pyrene-d10
34	100	82	97	1	1545900	vb	955	188 Anthracene-d10
35	100	80	97	0	247940	bb	488	240 1,4-Dibromobenzene-d4
36	87	63	87	1	452300	bb	430	185 1,3,5-Trichlorobenzene-

19-Sep-91 13:53
Sample: SSTD160

Triangle Labs, Inc.

(919) 544-5729
Instrument F



No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	76	98	1	138860	bb	305	152 1,4 Dichlorobenzene-d4
2	91	76	94	-1	589570	bb	481	136 Naphthalene-d8
3	100	93	97	1	2203200	bb	484	128 Naphthalene
4	100	92	98	0	1811900	bb	585	142 2-Methylnaphthalene
5	100	70	97	0	343650	bb	733	164 Acenaphthene-d10
6	100	95	98	1	1301800	bb	654	162 2-Chloronaphthalene
7	100	95	99	0	2149200	bb	711	152 Acenaphthylene
8	100	81	99	1	1431700	bb	738	153 Acenaphthene
9	100	91	95	1	1499500	bb	814	166 Fluorene
10	100	77	96	0	675180	vv	946	188 Phenanthrene-d10
11	100	94	98	1	2415300	bv	950	178 Phenanthrene
12	100	94	98	1	2263600	vb	958	178 Anthracene
13	100	94	97	1	2646400	vv	1123	202 Fluoranthene
14	77	51	93	2	769280	bb	1340	240 Chrysene-d12
15	100	90	98	-2	1853800	bb	1193	244 Terphenyl-d14
16	100	88	97	0	2745400	bb	1154	202 Pyrene
17	100	87	97	1	3229200	bv*	1339	228 Benzo(a)anthracene
18	100	89	100	1	2975900	vb	1345	228 Chrysene
19	93	81	92	2	1026200	vb	1560	264 Perylene-d12
20	100	92	95	1	3969500	v!*	1507	252 Benzo(b)fluoranthene
21	100	93	96	1	3693000	!b	1512	252 Benzo(k)fluoranthene
22	100	92	99	1	3782700	vv	1545	252 Benzo(e)pyrene
23	100	92	99	2	3818300	vv	1554	252 Benzo(a)pyrene
24	100	91	98	1	2255800	vv	1565	252 Perylene
25	100	93	97	2	3864800	bv	1708	276 Indeno(1,2,3-cd)pyrene
26	100	89	94	1	4173800	bv	1715	278 Dibenz(a,h)anthracene
27	100	93	95	2	4082100	b?	1740	276 Benzo(g,h,i)perylene
28	100	84	97	0	196480	bb	924	266 Pentachlorophenol
29	89	68	98	2	660900	bb	385	82 Nitrobenzene-d5
30	100	93	99	0	1178900	bb	646	172 2-Fluorobiphenyl
31	92	73	86	1	129500	bb	849	330 2,4,6-Tribromophenol
32	85	54	92	1	778800	bb	275	99 Phenol-d5
33	100	77	97	0	1996800	vb	1151	212 Pyrene-d10
34	100	82	98	2	1982900	vb	956	188 Anthracene-d10
35	100	81	95	-1	270030	bb	489	240 1,4-Dibromobenzene-d4
36	92	61	86	0	479280	bb	430	185 1,3,5-Trichlorobenzene-

19-Sep-91 12:08

Triangle Labs, Inc.

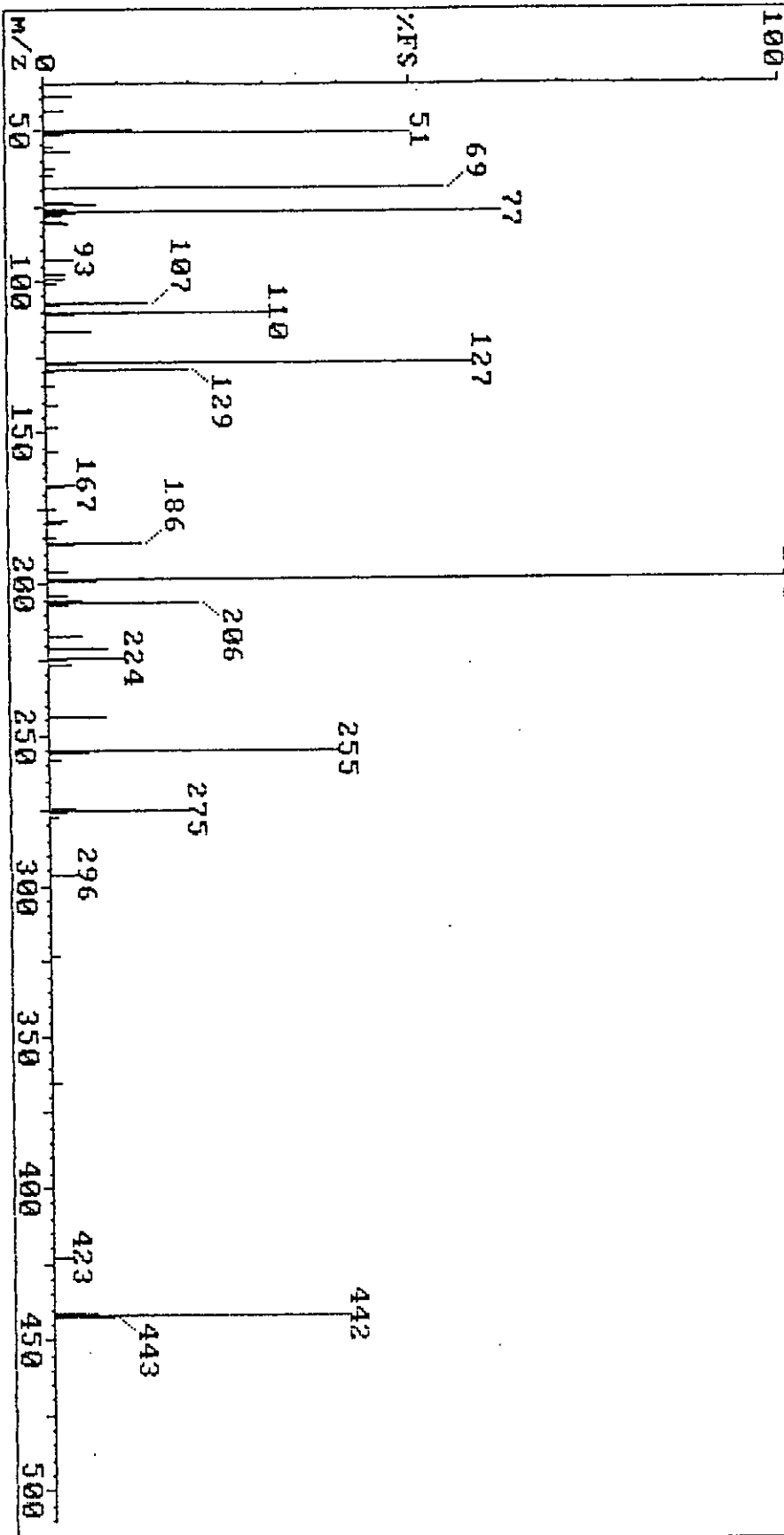
Sample: DFTPP

(919) 544-5729
Instrument F

FE806 396 (5.300)

198

52224



Pk#	Mass	Abs Int	Rel Int	Pk#	Mass	Abs Int	Rel Int	Pk#	Mass	Abs Int	Rel Int	Pk#	Mass	Abs Int	Rel Int	Pk#	Mass	Abs Int	Rel Int
1	39	2864	3.95	15	78	2384	4.41	29	128	2288	4.23	43	187	1728	3.31	57	255	28488	39.22
2	44	1392	2.67	16	79	1312	2.51	30	129	18112	19.36	44	196	1392	2.67	58	256	2864	5.48
3	58	6272	12.81	17	88	1128	2.14	31	138	648	1.23	45	198	52224	108.88	59	258	736	1.41
4	51	26112	58.88	18	81	1648	3.16	32	135	628	1.28	46	199	3488	6.68	60	274	1768	3.37
5	52	1368	2.68	19	93	1952	3.74	33	141	892	1.71	47	284	1392	2.67	61	275	9792	18.75
6	56	596	1.14	20	98	1392	2.67	34	148	848	1.61	48	285	2488	4.68	62	276	1216	2.33
7	57	1888	3.46	21	99	1448	2.76	35	156	848	1.62	49	286	18688	28.47	63	277	568	1.87
8	63	864	1.65	22	101	828	1.57	36	167	2832	3.89	50	287	1344	2.57	64	296	1792	3.43
9	65	516	0.99	23	107	7296	13.97	37	168	1216	2.33	51	217	2384	4.56	65	323	668	1.28
10	69	28416	54.41	24	108	1856	2.82	38	175	696	1.33	52	221	4288	8.21	66	365	696	1.33
11	74	2888	3.83	25	118	15936	38.51	39	179	1368	2.68	53	224	5312	10.17	67	423	1232	2.36
12	75	3688	6.89	26	111	1952	3.74	40	188	968	1.84	54	225	1264	2.42	68	441	3824	5.79
13	76	1632	3.13	27	117	3248	6.22	41	185	584	1.12	55	227	1696	3.25	69	442	28992	48.28
14	77	32512	62.25	28	127	38288	57.84	42	186	6728	12.87	56	244	4816	7.59	78	443	4288	8.21

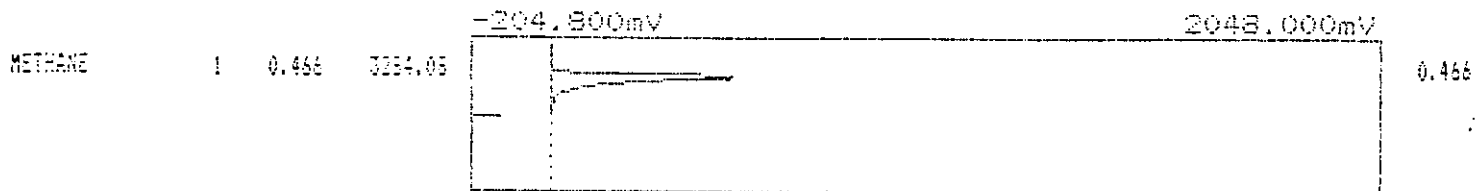
DFTPP TUNE CHECK REPORT

Raw Data File: FE806
 Date: 19-Sep-91
 Time: 12:08

M/E	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	50.00	PASS
68	Less than 2.0% of mass 69	0.00(0.0)1	PASS
69	Mass 69 relative abundance	54.41	PASS
70	Less than 2.0% of mass 69	0.00(0.0)1	PASS
127	40.0 - 60.0% of mass 198	57.84	PASS
197	Less than 1% of mass 198	0.00	PASS
198	Base peak, 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	6.68	PASS
275	10 - 30% of mass 198	18.75	PASS
365	Greater than 1% of mass 198	1.33	PASS
441	Present, but less than mass 443	5.79	PASS
442	Greater than 40% of mass 198	40.20	PASS
443	17 - 23% of mass 442	8.21(20.4)2	PASS

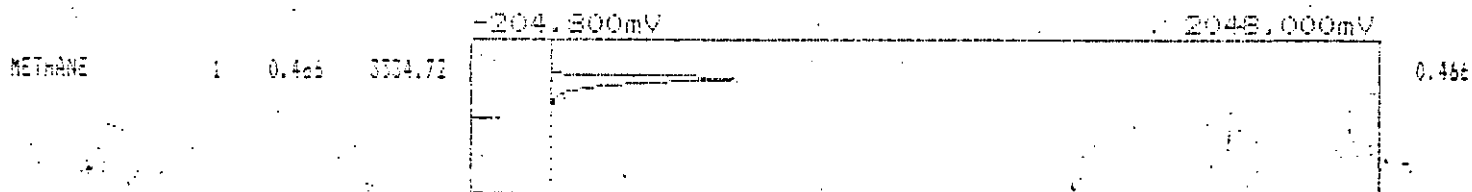
IX. CALIBRATIONS
B. GAS CHROMATOGRAPHY

Operator : RAMCON
 Instrument : Instrument 1
 File : LRMET3A.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Units
METHANE	1	0.466	499.815	3284.08	100.00	N/A	
	1			3284.08	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : LRMET3B.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Unit
METHANE	1	0.466	503.804	3334.72	100.00	N/A	
	1			3334.72	100.00	N/A	

PREPARATION OF STANDARDS IN TEDLAH BAGS AND CALIBRATION CURVE

STANDARDS

Standards Preparation Data:

Organic: BTEX
 Bag # or identification
 Dry gas meter calibration factor
 Final meter reading (liters)
 Initial meter reading (liters)
 Metered volume (liters)
 Avg. meter temperature (°K)
 Avg. meter pressure, gauge (mm Hg)
 Avg. atmospheric pressure (mm Hg)
 Avg. meter pressure, absolute (mm Hg)
 Syringe temperature (°K)
 Syringe pressure, absolute (mm Hg)
 Volume of gas in syringe (ml)
 Density of liquid organic (g/ml)
 Volume of liquid in syringe (μl)

Mixture #1	Mixture #2	Mixture #3
<u>Benzene</u>	<u>Toluene</u>	<u>Ethyl Benzene</u>
<u>1.99</u>	<u>1.99</u>	<u>1.99</u>
<u>50</u>	<u>50</u>	<u>50</u>
<u>0</u>	<u>0</u>	<u>0</u>
<u>50</u>	<u>50</u>	<u>50</u>
<u>299.64</u>	<u>299.64</u>	<u>299.64</u>
<u>26.02</u>	<u>26.02</u>	<u>26.02</u>
<u>762.26</u>	<u>762.26</u>	<u>762.26</u>
<u>788.28</u>	<u>788.28</u>	<u>788.28</u>
<u>---</u>	<u>---</u>	<u>---</u>
<u>---</u>	<u>---</u>	<u>---</u>
<u>---</u>	<u>---</u>	<u>---</u>
<u>.874</u>	<u>.865</u>	<u>.867</u>
<u>2.3</u>	<u>2</u>	<u>2.5</u>

GC Operating Conditions:

Sample loop volume (ml)
 Sample loop temperature (°C)
 Carrier gas flow rate (ml/min)
 Column temperature:
 Initial (°C)
 Rate change (°C/min)
 Final (°C)

<u>1</u>	<u>1</u>	<u>1</u>
<u>75</u>	<u>75</u>	<u>75</u>
<u>30</u>	<u>30</u>	<u>30</u>
<u>75</u>	<u>75</u>	<u>75</u>
<u>-</u>	<u>-</u>	<u>-</u>
<u>75</u>	<u>75</u>	<u>75</u>

Organic Peak Identification and Calculated Concentrations:

Injection time (24-hr clock)
 Distance to peak (cm)
 Chart speed (cm/min)
 Organic retention time (min)
 Attenuation factor
 Peak height (mm)
 Peak area (mm²)
 Peak area x attenuation factor (mm²)
 Calculated concentration (ppm)
 (Equation 18-3 or 18-4)

<u>1.55</u>	<u>2.94</u>	<u>5.38</u>
<u>1.55</u>	<u>2.94</u>	<u>5.38</u>
<u>16</u>	<u>16</u>	<u>16</u>
<u>17.537</u>	<u>11.840</u>	<u>7.932</u>
<u>160.56</u>	<u>158.60</u>	<u>157.25</u>
<u>2568.96</u>	<u>2537.6</u>	<u>2516</u>
<u>12.3</u>	<u>9.4</u>	<u>9.78</u>

Plot peak area x attenuation factor against calculated concentration to obtain calibration curve.

PREPARATION OF STANDARDS IN TEDLAR BAGS AND CALIBRATION CURVE

STANDARDS

Standards Preparation Data:	Mixture #1	Mixture #2	Mixture #3
Organic: _____	<u>Y. Hex</u>	_____	_____
Bag # or identification	_____	_____	_____
Dry gas meter calibration factor	<u>1.99</u>	_____	_____
Final meter reading (liters)	<u>50</u>	_____	_____
Initial meter reading (liters)	<u>0</u>	_____	_____
Metered volume (liters)	<u>50</u>	_____	_____
Avg. meter temperature (°K)	<u>299.64</u>	_____	_____
Avg. meter pressure, gauge (mm Hg)	<u>26.02</u>	_____	_____
Avg. atmospheric pressure (mm Hg)	<u>762.26</u>	_____	_____
Avg. meter pressure, absolute (mm Hg)	<u>788.28</u>	_____	_____
Syringe temperature (°K)	_____	_____	_____
Syringe pressure, absolute (mm Hg)	_____	_____	_____
Volume of gas in syringe (ml)	_____	_____	_____
Density of liquid organic (g/ml)	<u>0.860</u>	_____	_____
Volume of liquid in syringe (μl)	<u>58</u>	_____	_____

GC Operating Conditions:

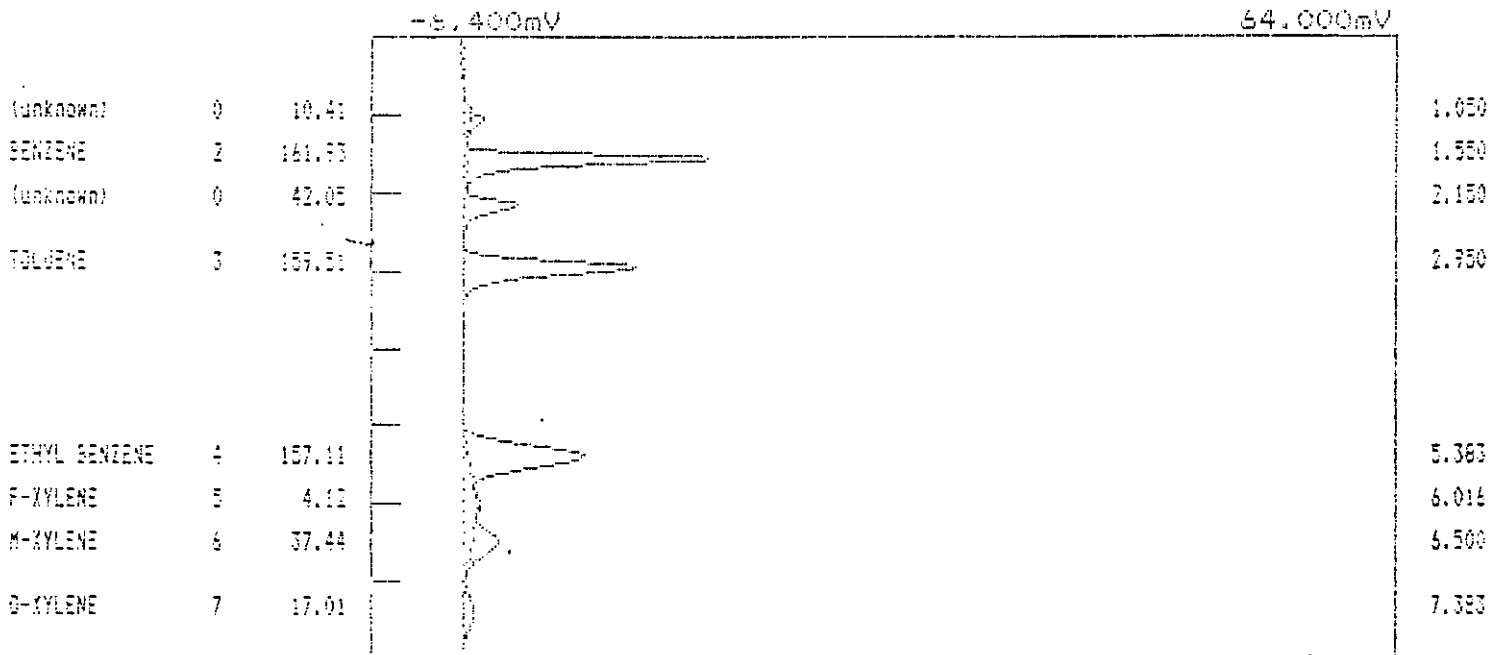
Sample loop volume (ml)	<u>1</u>	_____	_____
Sample loop temperature (°C)	<u>75</u>	_____	_____
Carrier gas flow rate (ml/min)	<u>30</u>	_____	_____
Column temperature:			
Initial (°C)	<u>75</u>	_____	_____
Rate change (°C/min)	<u>0</u>	_____	_____
Final (°C)	<u>75</u>	_____	_____

Organic Peak Identification and Calculated Concentrations:

Injection time (24-hr clock)	_____	_____	_____
Distance to peak (cm)	<u>60/65/73</u>	_____	_____
Chart speed (cm/min)	_____	_____	_____
Organic retention time (min)	<u>60/65/73</u>	_____	_____
Attenuation factor	<u>16</u>	_____	_____
Peak height (mm)	<u>60/65/73</u>	_____	_____
Peak area (mm ²)	<u>57.01</u>	_____	_____
Peak area x attenuation factor (mm ²)	<u>912.16</u>	_____	_____
Calculated concentration (ppm)	<u>3.1</u>	_____	_____
(Equation 18-3 or 18-4)			

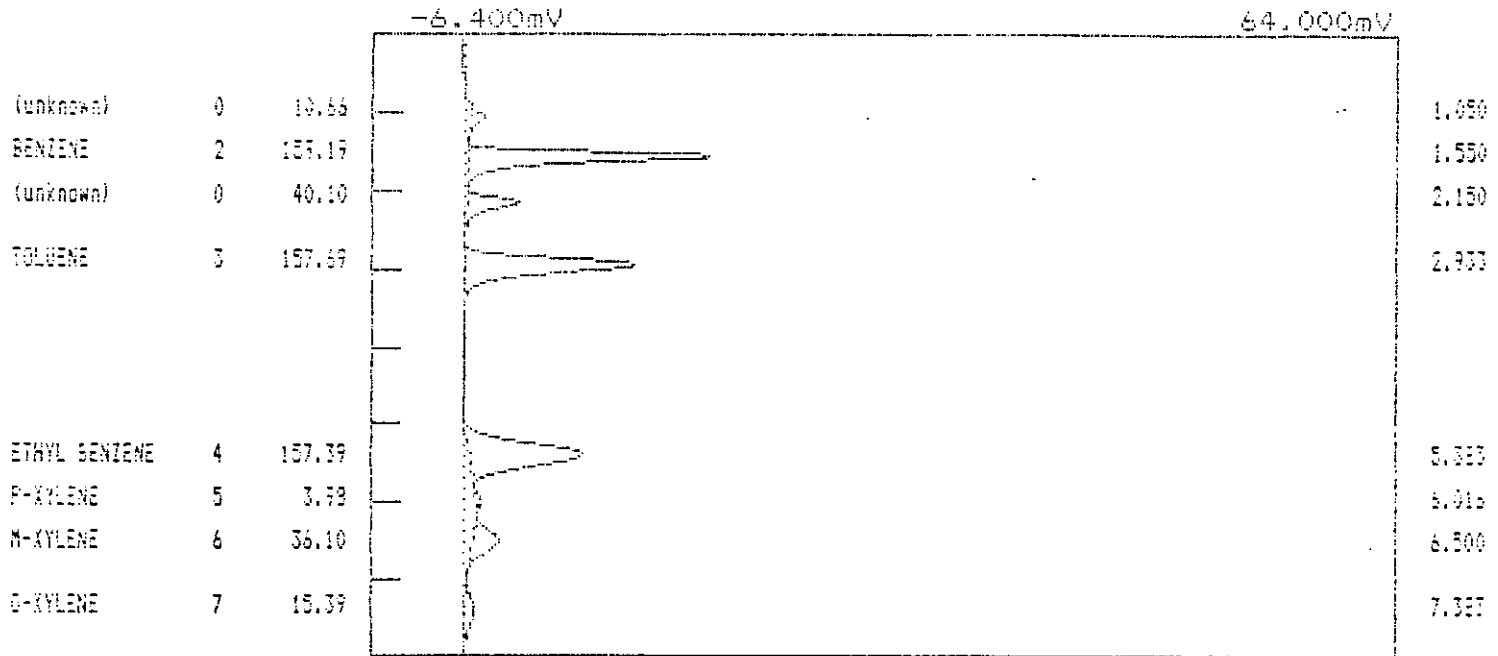
Plot peak area x attenuation factor against calculated concentration to obtain a curve.

Operator : RAMCON
 Instrument : Instrument 1
 File : CAL10A.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



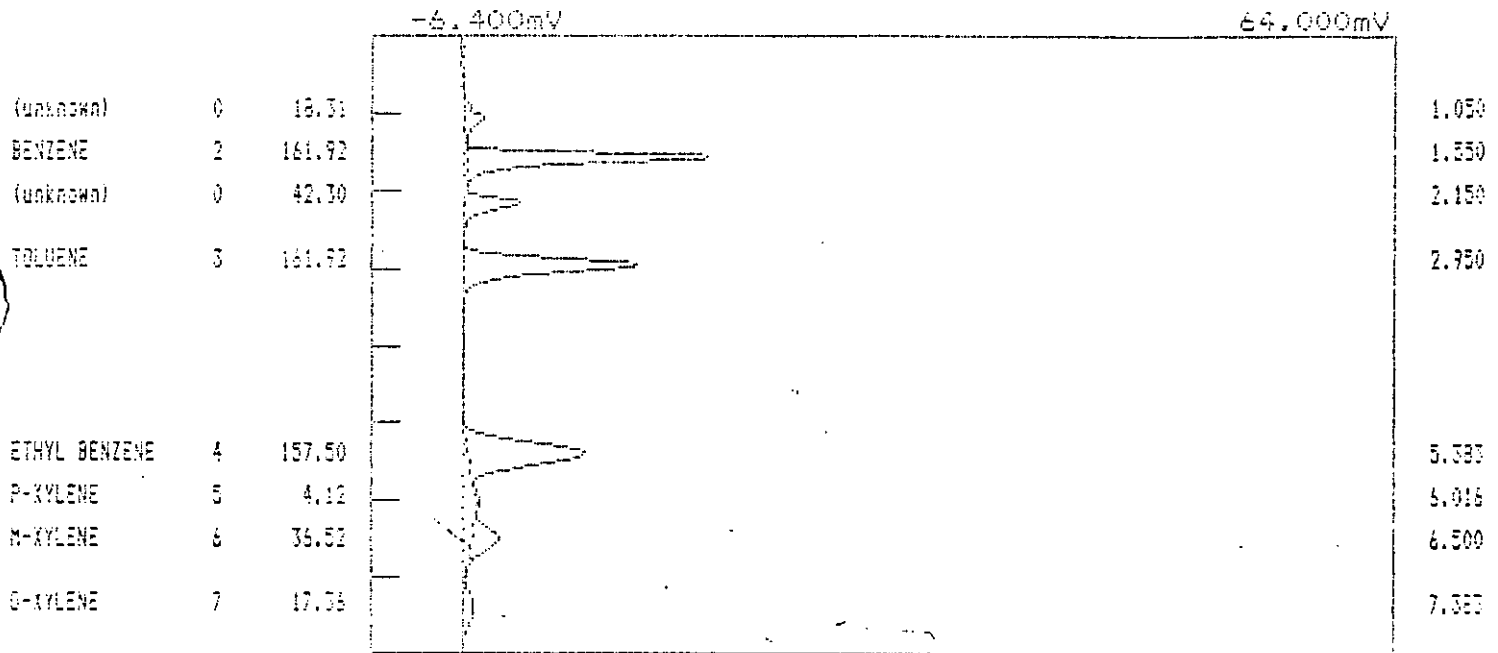
Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.550	17.626	161.93	27.47	N/A	
TOLUENE	3	2.950	11.920	159.51	27.05	N/A	
ETHYL BENZENE	4	5.383	7.960	157.11	26.65	N/A	
P-XYLENE	5	6.016	0.346	4.12	0.70	N/A	
M-XYLENE	6	6.500	1.793	37.44	6.35	N/A	
O-XYLENE	7	7.333	0.680	17.01	2.89	N/A	
	6			537.12	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : CAL10B.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



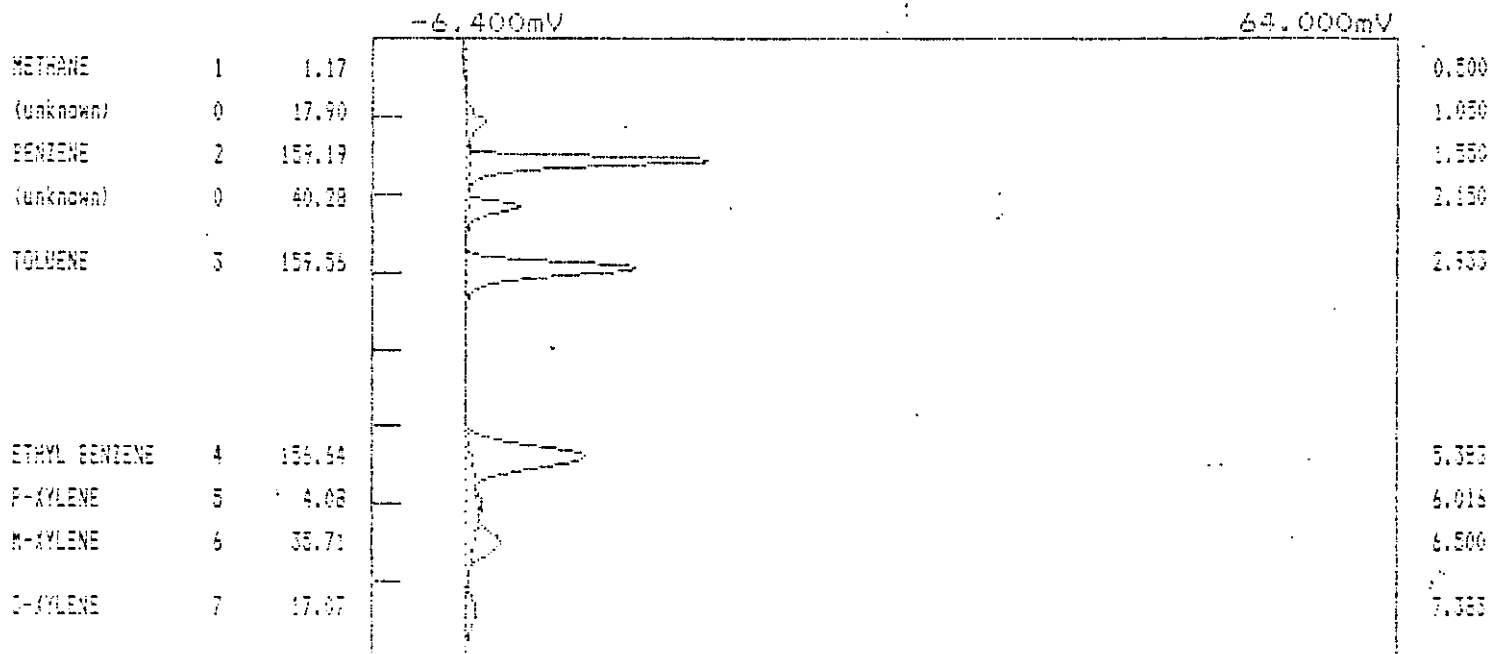
Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.550	17.446	1597.119	27.42	N/A	
TOLUENE	3	1.933	11.724	1027.409	27.16	N/A	
ETHYL BENZENE	4	3.854	7.914	697.409	17.11	N/A	
P-XYLENE	5	6.016	0.337	2.919	0.08	N/A	
M-XYLENE	6	6.500	1.773	155.110	3.63	N/A	
O-XYLENE	7	7.683	0.660	57.510	1.38	N/A	
	6			529.74	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : KCAL10A.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	161.92	17.6226	161.92	26.99	N/A	
TOLUENE	3	161.92	11.9436	161.92	26.99	N/A	
ETHYL BENZENE	4	157.50	7.6436	157.50	26.99	N/A	
P-KYLENE	5	4.12	0.046	4.12	0.69	N/A	
M-KYLENE	6	36.52	4.793	36.52	6.09	N/A	
O-KYLENE	7	17.36	0.683	17.36	2.89	N/A	
	6			539.34	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : KCAL108.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Unit
METHANE	1	0.500	0.17	1.17	0.20	N/A	
BENZENE	2	1.900	17.42	11.77	2.01	N/A	
TOLUENE	3	159.000	11.77	15.04	2.67	N/A	
ETHYL BENZENE	4	156.000	7.77	10.04	1.80	N/A	
P-XYLENE	5	4.000	0.04	0.04	0.00	N/A	
M-XYLENE	6	35.000	0.04	0.04	0.00	N/A	
O-XYLENE	7	17.000	0.04	0.04	0.00	N/A	
	7			533.42	100.00	N/A	

PREPARATION OF STANDARDS IN TEDLAR BAGS AND CALIBRATION CURVE

STANDARDS

Standards Preparation Data:

	Mixture #1	Mixture #2	Mixture #3
Organic: <u>BTEX</u>	<u>Benzene</u>	<u>Toluene</u>	<u>Ethyl Benzene</u>
Bag # or identification			
Dry gas meter calibration factor	<u>1.99</u>	<u>1.99</u>	<u>1.99</u>
Final meter reading (liters)	<u>50</u>	<u>50</u>	<u>50</u>
Initial meter reading (liters)	<u>0</u>	<u>0</u>	<u>0</u>
Metered volume (liters)	<u>50</u>	<u>50</u>	<u>50</u>
Avg. meter temperature (°K)	<u>299.64</u>	<u>299.64</u>	<u>299.64</u>
Avg. meter pressure, gauge (mm Hg)	<u>26.02</u>	<u>26.02</u>	<u>26.02</u>
Avg. atmospheric pressure (mm Hg)	<u>762.26</u>	<u>762.26</u>	<u>762.26</u>
Avg. meter pressure, absolute (mm Hg)	<u>788.28</u>	<u>788.28</u>	<u>788.28</u>
Syringe temperature (°K)			
Syringe pressure, absolute (mm Hg)			
Volume of gas in syringe (ml)			
Density of liquid organic (g/ml)	<u>0.874</u>	<u>0.865</u>	<u>0.867</u>
Volume of liquid in syringe (μ l)	<u>6.5</u>	<u>6</u>	<u>6.5</u>

GC Operating Conditions:

Sample loop volume (ml)	<u>1</u>	<u>1</u>	<u>1</u>
Sample loop temperature (°C)	<u>75</u>	<u>75</u>	<u>75</u>
Carrier gas flow rate (ml/min)	<u>30</u>	<u>30</u>	<u>30</u>
Column temperature:			
Initial (°C)	<u>75</u>	<u>75</u>	<u>75</u>
Rate change (°C/min)	<u>-</u>	<u>-</u>	<u>-</u>
Final (°C)	<u>75</u>	<u>75</u>	<u>75</u>

Organic Peak Identification and Calculated Concentrations:

Injection time (24-hr clock)			
Distance to peak (cm)	<u>1.5</u>	<u>2.9</u>	<u>6.4</u>
Chart speed (cm/min)			
Organic retention time (min)	<u>1.5</u>	<u>2.9</u>	<u>6.4</u>
Attenuation factor	<u>16</u>	<u>16</u>	<u>16</u>
Peak height (mm)	<u>48.9</u>	<u>36.4</u>	<u>11.25</u>
Peak area (mm ²)	<u>444.8</u>	<u>483.60</u>	<u>648.57</u>
Peak area x attenuation factor (mm ²)	<u>7116.8</u>	<u>7737.6</u>	<u>10377.12</u>
Calculated concentration (ppm)	<u>34.8</u>	<u>26.9</u>	<u>41</u>
(Equation 18-3 or 18-4)			

Plot peak area x attenuation factor against calculated concentration to obtain calibration curve.

PREPARATION OF STANDARDS IN TEDLAR BAGS AND CALIBRATION CURVE

STANDARDS

Standards Preparation Data:

	Mixture #1	Mixture #2	Mixture #3
Organic: <u>Xylene</u>	<u>Xylene</u>	<u> </u>	<u> </u>
Bag # or identification	<u> </u>	<u> </u>	<u> </u>
Dry gas meter calibration factor	<u>1.99</u>	<u> </u>	<u> </u>
Final meter reading (liters)	<u>50</u>	<u> </u>	<u> </u>
Initial meter reading (liters)	<u>0</u>	<u> </u>	<u> </u>
Metered volume (liters)	<u>50</u>	<u> </u>	<u> </u>
Avg. meter temperature (°K)	<u>299.64</u>	<u> </u>	<u> </u>
Avg. meter pressure, gauge (mm Hg)	<u>26.02</u>	<u> </u>	<u> </u>
Avg. atmospheric pressure (mm Hg)	<u>762.26</u>	<u> </u>	<u> </u>
Avg. meter pressure, absolute (mm Hg)	<u>788.28</u>	<u> </u>	<u> </u>
Syringe temperature (°K)	<u> </u>	<u> </u>	<u> </u>
Syringe pressure, absolute (mm Hg)	<u> </u>	<u> </u>	<u> </u>
Volume of gas in syringe (ml)	<u> </u>	<u> </u>	<u> </u>
Density of liquid organic (g/ml)	<u>0.860</u>	<u> </u>	<u> </u>
Volume of liquid in syringe (μl)	<u>5.5</u>	<u> </u>	<u> </u>

GC Operating Conditions:

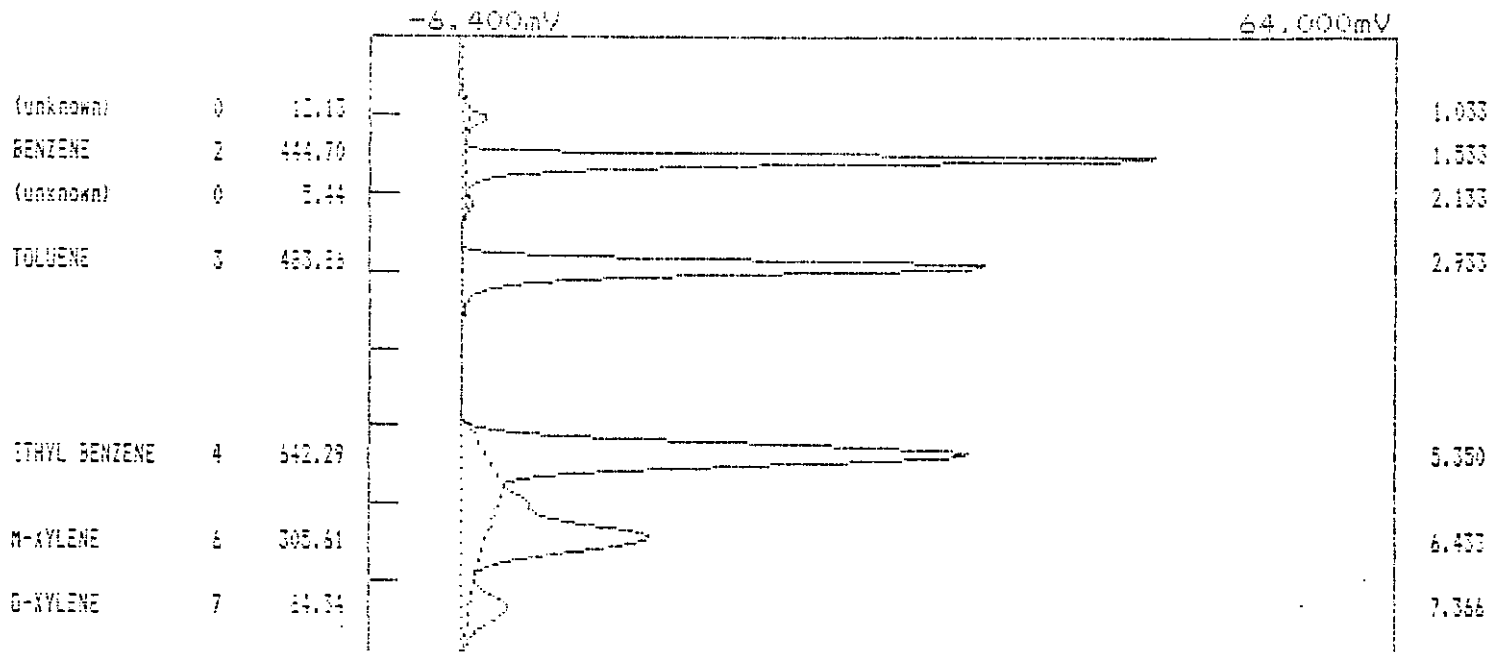
Sample loop volume (ml)	<u>1</u>	<u> </u>	<u> </u>
Sample loop temperature (°C)	<u>75</u>	<u> </u>	<u> </u>
Carrier gas flow rate (ml/min)	<u>30</u>	<u> </u>	<u> </u>
Column temperature:			
Initial (°C)	<u>75</u>	<u> </u>	<u> </u>
Rate change (°C/min)	<u> </u>	<u> </u>	<u> </u>
Final (°C)	<u>75</u>	<u> </u>	<u> </u>

Organic Peak Identification and Calculated Concentrations:

Injection time (24-hr clock)	<u> </u>	<u> </u>	<u> </u>
Distance to peak (cm)	<u>647.3</u>	<u> </u>	<u> </u>
Chart speed (cm/min)	<u> </u>	<u> </u>	<u> </u>
Organic retention time (min)	<u>647.3</u>	<u> </u>	<u> </u>
Attenuation factor	<u>16</u>	<u> </u>	<u> </u>
Peak height (mm)	<u>1132.5</u>	<u> </u>	<u> </u>
Peak area (mm ²)	<u>372.84</u>	<u> </u>	<u> </u>
Peak area x attenuation factor (mm ²)	<u> </u>	<u> </u>	<u> </u>
Calculated concentration (ppm) (Equation 18-3 or 18-4)	<u>21.3</u>	<u> </u>	<u> </u>

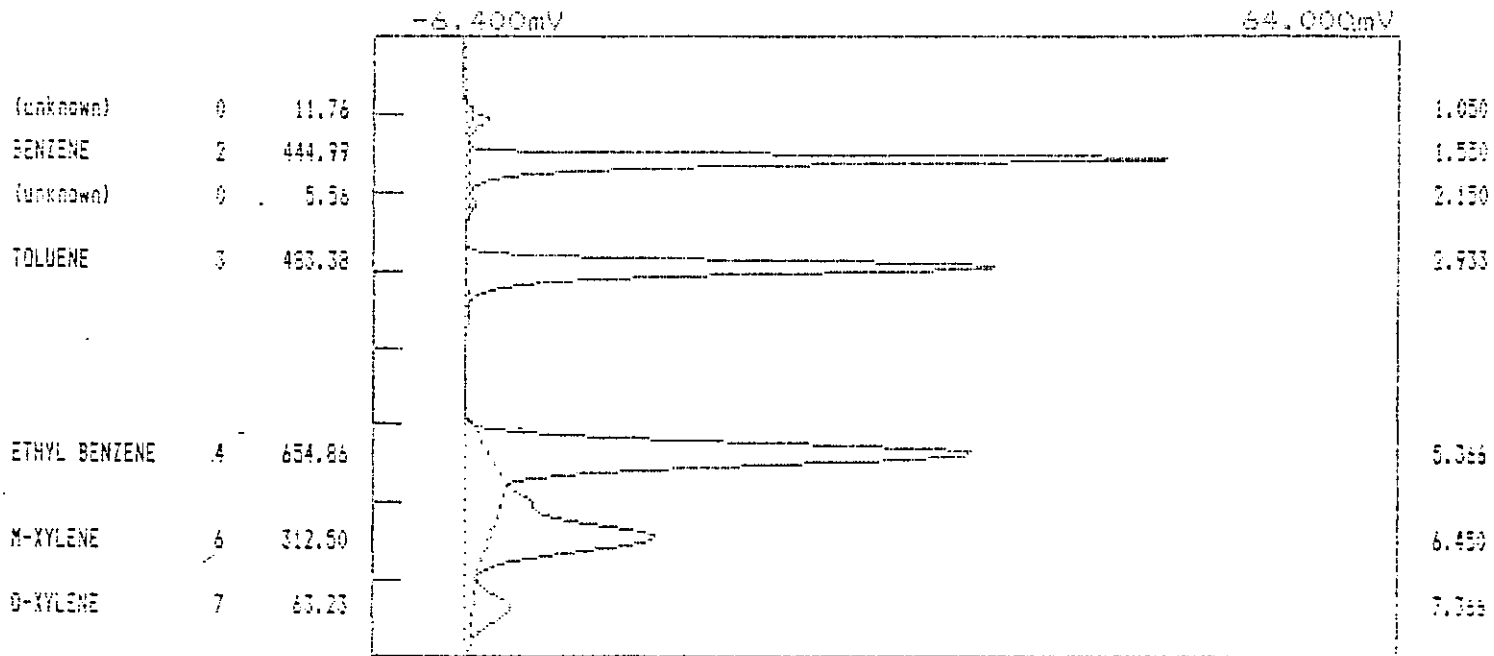
Plot peak area x attenuation factor against calculated concentration to obtain calibration curve.

Operator : RAMCON
 Instrument : Instrument 1
 File : CAL50B.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



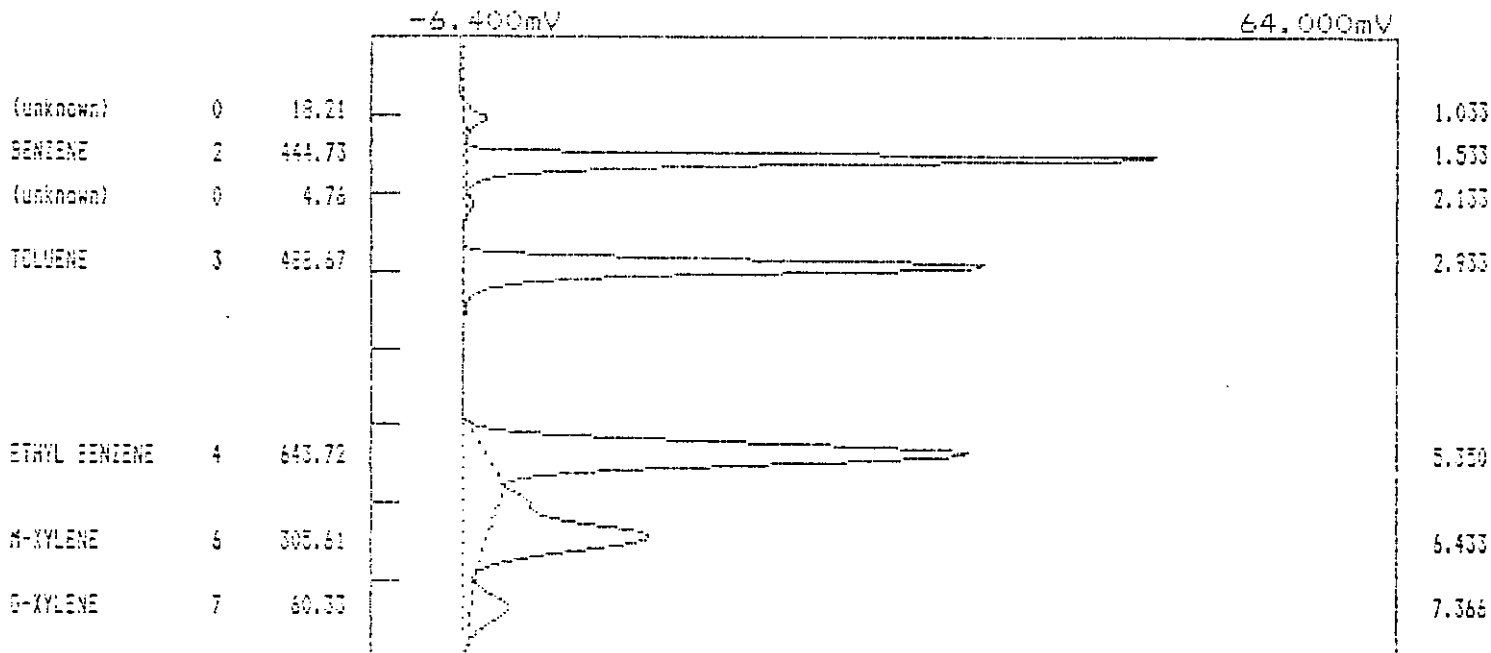
Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.8333	48.653	444.70	32.71	N/A	
TOLUENE	3	2.9333	34.031	483.23	34.71	N/A	
ETHYL BENZENE	4	3.9333	36.043	642.29	46.80	N/A	
m-XYLENE	6	6.4333	11.207	305.61	10.61	N/A	
o-XYLENE	7	7.3666	2.843	64.34	3.29	N/A	
	5			1940.80	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : CALSOC.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



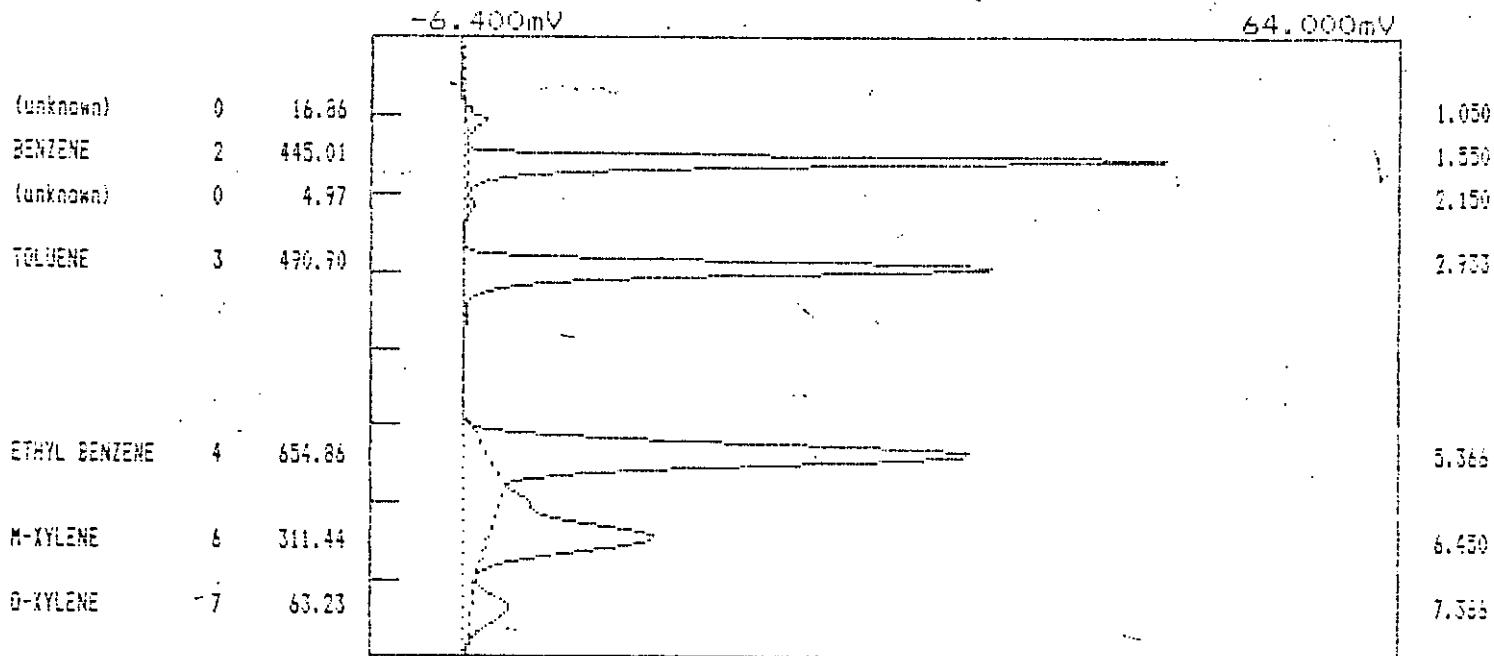
Component	Number	Retention	Height	Area	Area %	External	Unit
BENZENE	1	444.97	444.97	444.97	100.00	N/A	
TOLUENE	2	453.38	453.38	453.38	100.00	N/A	
ETHYL BENZENE	3	654.86	654.86	654.86	100.00	N/A	
M-XYLENE	4	312.50	312.50	312.50	100.00	N/A	
P-XYLENE	5	63.23	63.23	63.23	100.00	N/A	
	5			1958.96	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : KCAL50B.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.533	46.956	444.73	22.62	N/A	
TOLUENE	3	2.933	36.424	488.67	24.86	N/A	
ETHYL BENZENE	4	5.350	33.070	643.72	32.74	N/A	
m-XYLENE	6	6.433	11.207	305.61	15.54	N/A	
p-XYLENE	7	7.366	2.515	60.33	3.07	N/A	
	5			1943.05	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : KCAL50C.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Unit
BENZENE	2	1.550	49.369	445.01	22.39	N/A	
TOLUENE	3	2.933	36.600	470.70	24.70	N/A	
ETHYL BENZENE	4	5.366	30.501	654.86	32.95	N/A	
M-XYLENE	6	6.450	11.382	311.44	15.67	N/A	
O-XYLENE	7	7.366	2.546	63.23	3.18	N/A	
	5			1965.45	100.00	N/A	

PREPARATION OF STANDARDS IN TEDLAR BAGS AND CALIBRATION CURVE

STANDARDS

Standards Preparation Data:

	Mixture #1	Mixture #2	Mixture #3
Organic: <u>BTEX</u>	<u>Benzene</u>	<u>Toluene</u>	<u>E. Benzene</u>
Bag # or identification			
Dry gas meter calibration factor	<u>1.99</u>	<u>1.99</u>	<u>1.99</u>
Final meter reading (liters)	<u>50</u>	<u>50</u>	<u>50</u>
Initial meter reading (liters)	<u>0</u>	<u>0</u>	<u>0</u>
Metered volume (liters)	<u>50</u>	<u>50</u>	<u>50</u>
Avg. meter temperature (°K)	<u>299.64</u>	<u>299.64</u>	<u>299.64</u>
Avg. meter pressure, gauge (mm Hg)	<u>26.02</u>	<u>26.02</u>	<u>26.02</u>
Avg. atmospheric pressure (mm Hg)	<u>762.26</u>	<u>762.26</u>	<u>762.26</u>
Avg. meter pressure, absolute (mm Hg)	<u>788.28</u>	<u>788.28</u>	<u>788.28</u>
Syringe temperature (°K)			
Syringe pressure, absolute (mm Hg)			
Volume of gas in syringe (ml)			
Density of liquid organic (g/ml)	<u>.874</u>	<u>.865</u>	<u>.867</u>
Volume of liquid in syringe (μ l)	<u>1</u>	<u>1.5</u>	<u>2</u>

GC Operating Conditions:

Sample loop volume (ml)	<u>1</u>	<u>1</u>	<u>1</u>
Sample loop temperature (°C)	<u>75</u>	<u>75</u>	<u>75</u>
Carrier gas flow rate (ml/min)	<u>30</u>	<u>30</u>	<u>30</u>
Column temperature:			
Initial (°C)	<u>75</u>	<u>75</u>	<u>75</u>
Rate change (°C/min)	<u>-</u>	<u>-</u>	<u>-</u>
Final (°C)	<u>75</u>	<u>75</u>	<u>75</u>

Organic Peak Identification and Calculated Concentrations:

Injection time (24-hr clock)			
Distance to peak (cm)	<u>1.5</u>	<u>2.9</u>	<u>5.3</u>
Chart speed (cm/min)			
Organic retention time (min)	<u>1.5</u>	<u>2.9</u>	<u>5.3</u>
Attenuation factor	<u>16</u>	<u>16</u>	<u>16</u>
Peak height (mm)	<u>10.2</u>	<u>7.2</u>	<u>6.2</u>
Peak area (mm ²)	<u>63.419</u>	<u>95.24</u>	<u>122.58</u>
Peak area x attenuation factor (mm ²)	<u>1015.84</u>	<u>1523.84</u>	<u>1961.28</u>
Calculated concentration (ppm)	<u>5.3</u>	<u>6.7</u>	<u>7.8</u>
(Equation 18-3 or 18-4)			

Plot peak area x attenuation factor against calculated concentration to obtain calibration curve.

PREPARATION OF STANDARDS IN TEDLAR BAGS AND CALIBRATION CURVE

STANDARDS

Standards Preparation Data:

	Mixture #1	Mixture #2	Mixture #3
Organic: <u>Xylene</u>			
Bag # or identification			
Dry gas meter calibration factor	<u>1.99</u>		
Final meter reading (liters)	<u>50</u>		
Initial meter reading (liters)	<u>0</u>		
Metered volume (liters)	<u>50</u>		
Avg. meter temperature (°K)	<u>299.64</u>		
Avg. meter pressure, gauge (mm Hg)	<u>26.02</u>		
Avg. atmospheric pressure (mm Hg)	<u>767.26</u>		
Avg. meter pressure, absolute (mm Hg)	<u>788.28</u>		
Syringe temperature (°K)			
Syringe pressure, absolute (mm Hg)			
Volume of gas in syringe (ml)			
Density of liquid organic (g/ml)	<u>.865</u>		
Volume of liquid in syringe (μl)	<u>.6</u>		

GC Operating Conditions:

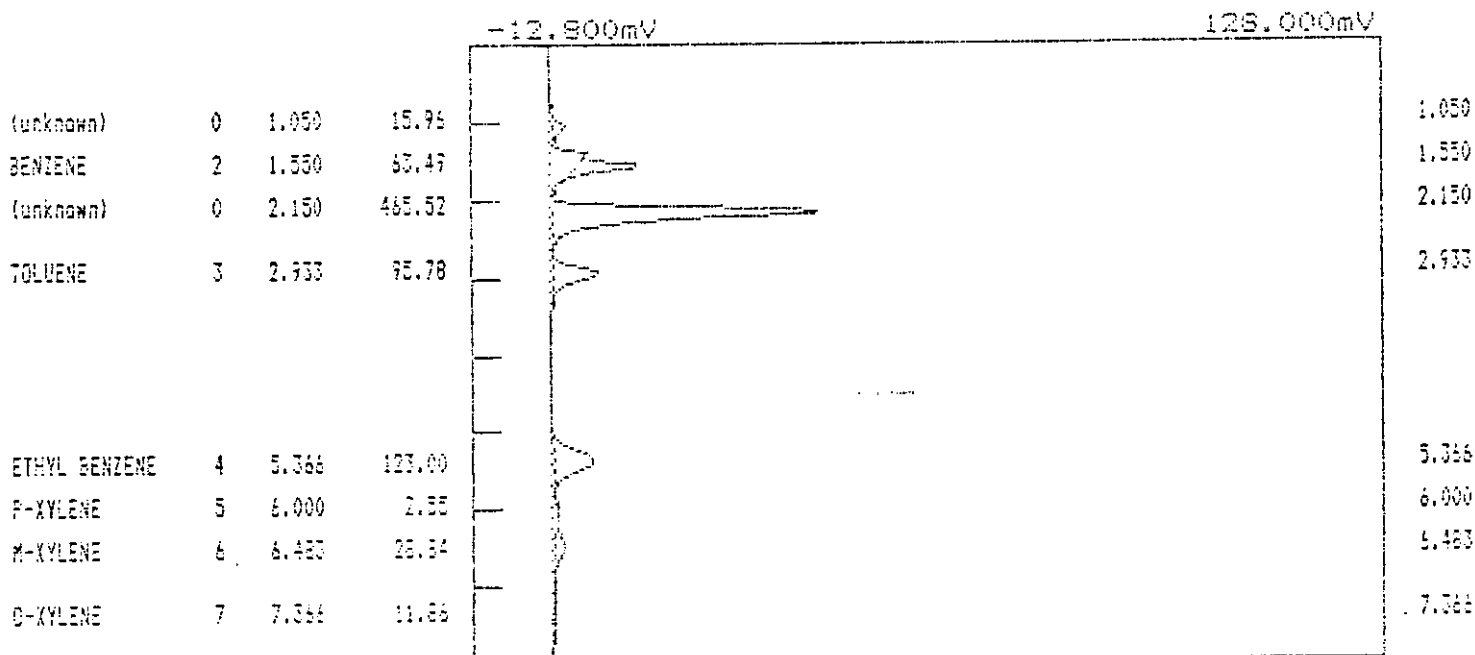
Sample loop volume (ml)	<u>1</u>		
Sample loop temperature (°C)	<u>75</u>		
Carrier gas flow rate (ml/min)	<u>30</u>		
Column temperature:			
Initial (°C)	<u>75</u>		
Rate change (°C/min)	<u>-</u>		
Final (°C)	<u>75</u>		

Organic Peak Identification and Calculated Concentrations:

Injection time (24-hr clock)			
Distance to peak (cm)	<u>59/64/73</u>		
Chart speed (cm/min)			
Organic retention time (min)	<u>59/64/73</u>		
Attenuation factor	<u>16</u>		
Peak height (mm)	<u>2/13/4</u>		
Peak area (mm ²)	<u>42.45</u>		
Peak area x attenuation factor (mm ²)	<u>679.2</u>		
Calculated concentration (ppm)	<u>2.3</u>		
(Equation 18-3 or 18-4)			

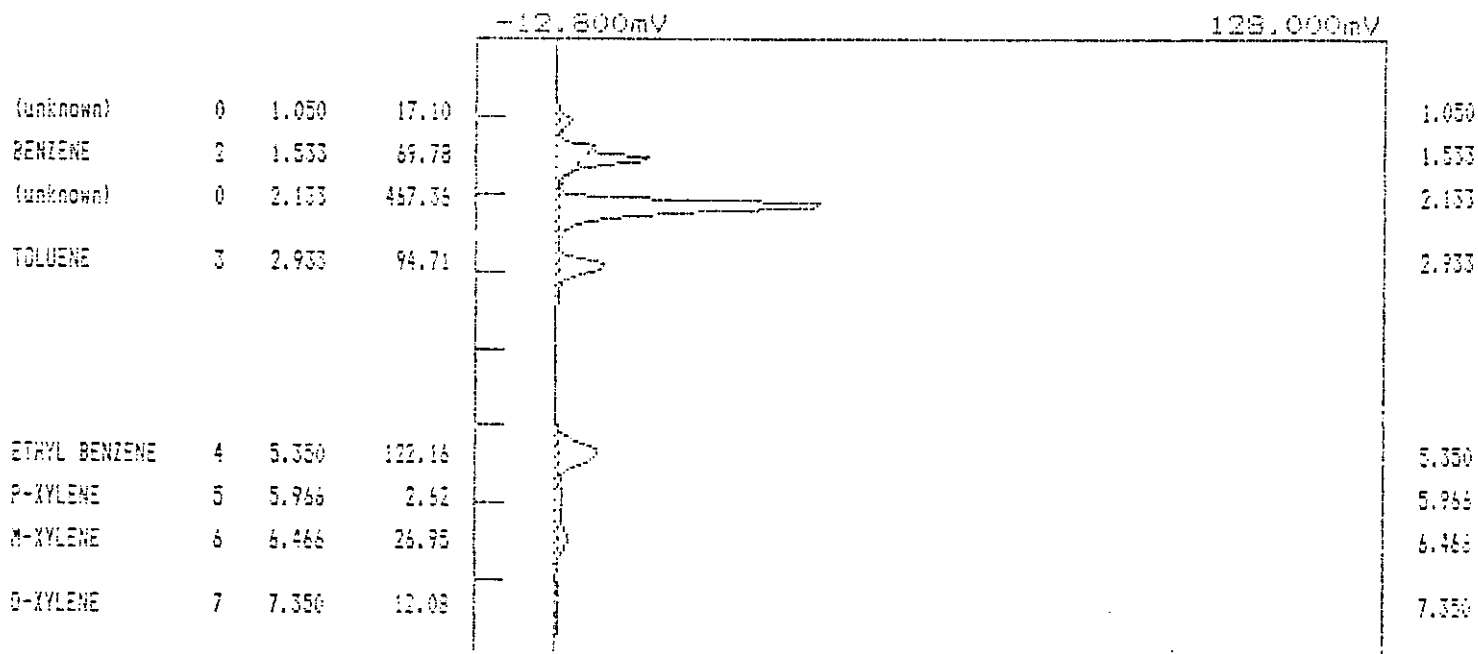
Plot peak area x attenuation factor against calculated concentration to obtain calibration curve.

Operator : RAMCON
 Instrument : Instrument 1
 File : CAL20A.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



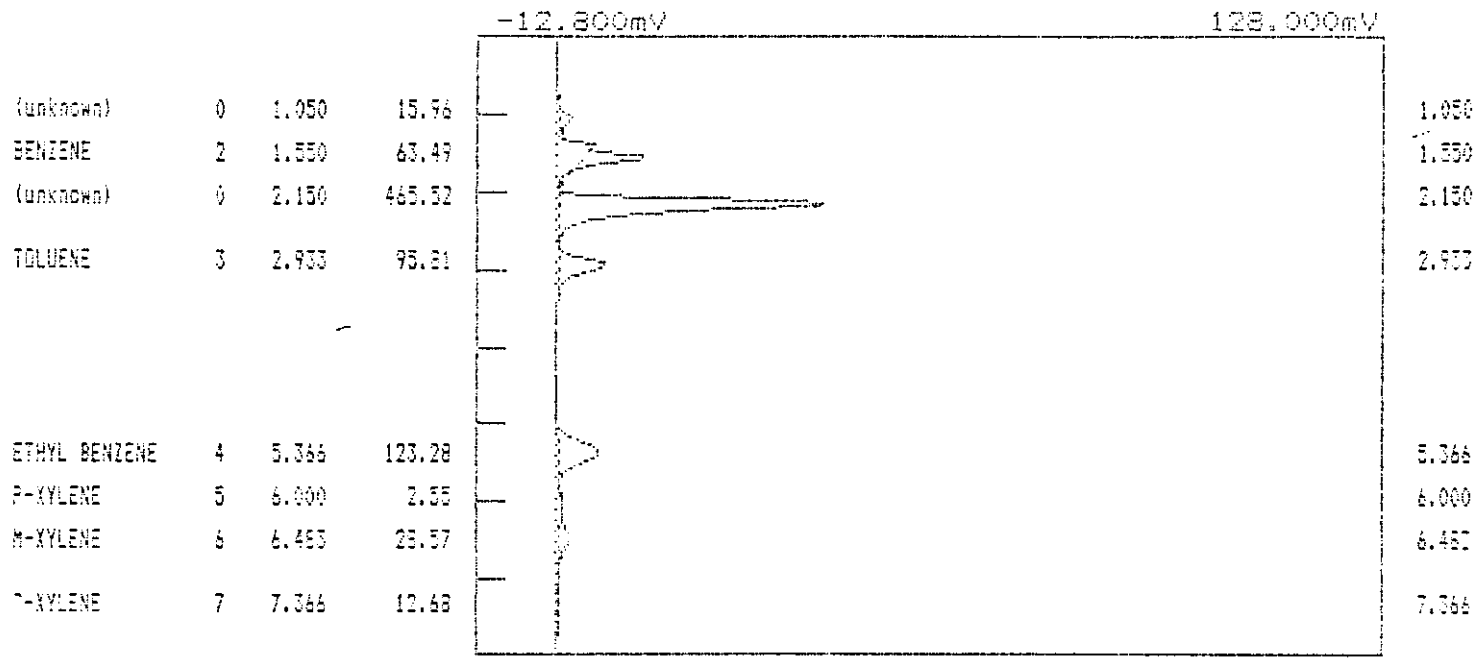
Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.550	10.1506	607.459	7.830	N/A	
TOLUENE	3	2.933	7.22006	905.739	11.77	N/A	
ETHYL BENZENE	4	5.366	6.50048	123.000	15.83	N/A	
P-XYLENE	5	6.000	0.22000	2.35000	0.03	N/A	
M-XYLENE	6	6.483	1.37400	26.3400	0.04	N/A	
O-XYLENE	7	7.366	0.49300	11.8500	1.55	N/A	
	6			325.51	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : CAL20B.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.533	10.272	69.78	100.00	N/A	
TOLUENE	3	2.933	7.230	94.71	100.00	N/A	
ETHYL BENZENE	4	5.350	0.209	122.16	100.00	N/A	
P-XYLENE	5	5.966	0.251	2.62	100.00	N/A	
M-XYLENE	6	6.466	1.501	26.95	100.00	N/A	
O-XYLENE	7	7.350	0.490	12.08	100.00	N/A	
	6			328.29	100.00	N/A	

Operator : RAMCON
 Instrument : Instrument 1
 File : KCAL20A.CHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT

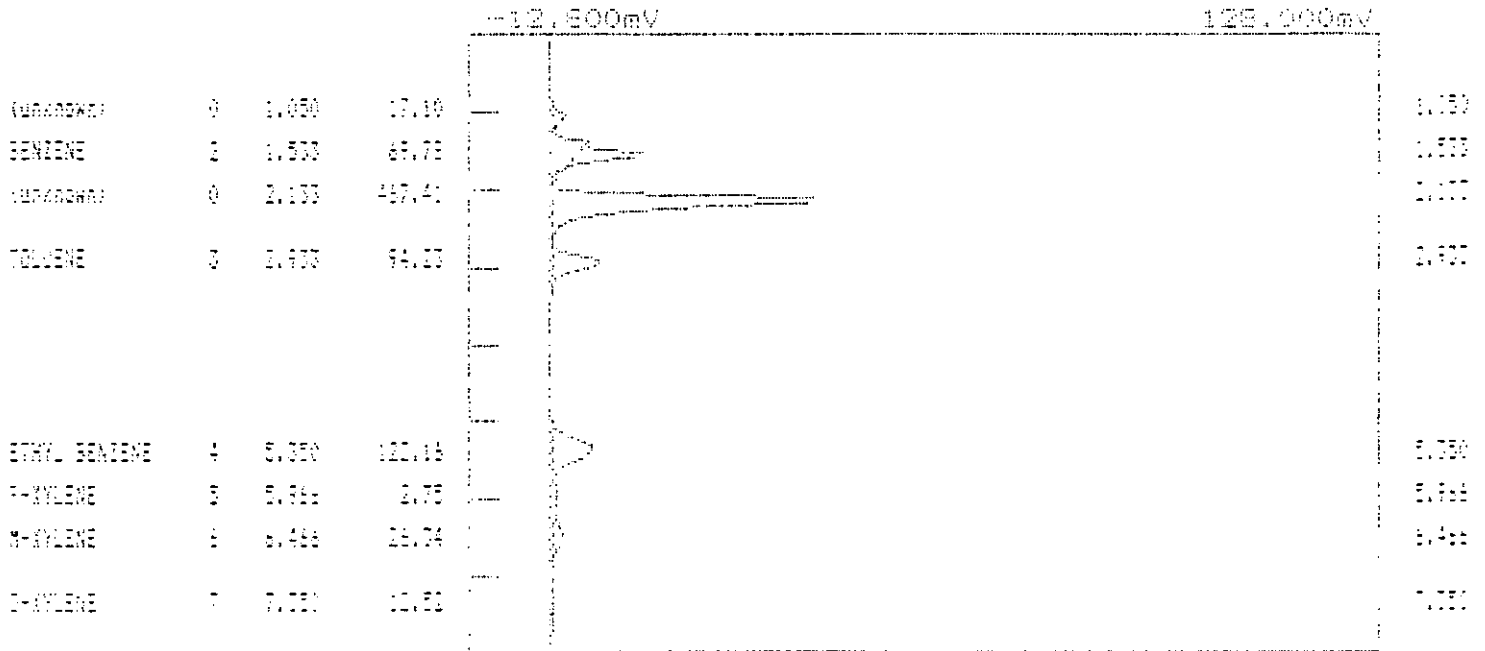


(unknown)	0	1.050	15.96
BENZENE	2	1.550	63.49
(unknown)	0	2.150	465.32
TOLUENE	3	2.933	95.81
ETHYL BENZENE	4	5.366	123.28
P-XYLENE	5	6.000	2.55
M-XYLENE	6	6.453	23.57
O-XYLENE	7	7.366	12.68

1.050
1.550
2.150
2.933
5.366
6.000
6.453
7.366

Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.550	10.166	36.464	7.79	N/A	
TOLUENE	3	2.933	7.606	12.484	11.75	N/A	
ETHYL BENZENE	4	5.366	6.406	10.094	10.13	N/A	
P-XYLENE	5	6.000	0.406	0.204	0.21	N/A	
M-XYLENE	6	6.453	1.406	2.004	1.91	N/A	
O-XYLENE	7	7.366	0.806	1.204	1.05	N/A	
	6			326.38	100.00	N/A	

Operator : RAMCOB
 Instrument : Instrument 1
 File : KCAL20B.DHR
 Temperature : BTEX.TEM
 Components : BTEX.CPT



Component	Number	Retention	Height	Area	Area %	External	Units
BENZENE	2	1.500	65.73			N/A	1.500
TOLUENE	3	2.600	54.23			N/A	2.600
ETHYL BENZENE	4	5.050	120.15			N/A	5.050
P-XYLENE	5	5.950	2.70			N/A	5.950
M-XYLENE	6	6.400	25.04			N/A	6.400
O-XYLENE	7	7.350	10.50			N/A	7.350
6				317.78	100.00	N/A	

IX. CALIBRATIONS

C. INSTRUMENTAL

INSTRUMENTAL ANALYSIS CALIBRATION DATA

CARBON MONOXIDE

Plant Lehman-Roberts

Location Memphis TN

Date 9-3-91

Operator KA

CO Range 1000

Initial Calibration: (Accuracy: \pm 5% Span)

Gas Type	Actual Concentration	Anayzer Response
CO-Zero	0	.7
CO-High	581	976.5
CO-Mid	598	612.5
CO-Low	328	314.5

Zero & Span Drift: (Accuracy \pm 5% Span)

End Run # / Time: 11:25-12:25

Gas Type	Initial Response	Final Response	Drift
CO-Zero	.7	-.5	
CO-	612.5	610.5	

End Run # 2 Time: 14:25-15:25

Gas Type	Initial Response	Final Response	Drift
CO-Zero	-.5	-.3	
CO-	610.5	616.7	

End Run # 3 Time: 16:33-17:33

Gas Type	Initial Response	Final Response	Drift
CO-Zero	-.3	-.6	
CO-	616.7	611.4	

End Run # Time:

Gas Type	Initial Response	Final Response	Drift
CO-Zero			
CO-			

INSTRUMENTAL ANALYSIS CALIBRATION DATA

DILUENT O₂ AND CO₂ MONITORS

Plant Lehrman - Roberts

Location Memphis TN

Date 9-3-91

Operator MA

Initial Calibration (Accuracy: ± 2% Span)

O ₂			CO ₂		
Gas Type	Actual Concentration	Analyzer Response	Gas Type	Actual Concentration	Analyzer Response
O ₂ -Zero	0.0	0.0	CO ₂ -Zero	0.0	0.1
O ₂ -High	20.9	20.9	CO ₂ -High	17.6	18.2
O ₂ -Mid	10.2	10.2	CO ₂ -Mid	14.5	10.2

System Bias Reponse: Analyzer Response-Initial Bias = ± 5% Span

Final Bias - Initial Bias = ± 3% Span

Run # 1 Time: 11:25-12:25

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.1	0.0	0.1	0.0	
CO ₂ /O ₂	10.2	10.2	10.0	10.0	

Run # 2 Time: 14:25-15:25

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.1	0.0	0.1	0.0	
CO ₂ /O ₂	10.0	10.0	10.1	10.0	

Run # 3 Time: 16:33-17:33

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.1	0.0	0.0	-0.1	
CO ₂ /O ₂	10.1	10.0	10.1	10.0	

Run # Time:

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero					
CO ₂ /O ₂					

INSTRUMENTAL ANALYSIS CALIBRATION DATA

TOTAL HYDROCARBONS

PLANT Lebanon-Roberts LOCATION Memphis TN
 DATE 5-3-91 OPERATOR A
 HC RANGE 1000 RESPONSE TIME _____

INITIAL CALIBRATION: (Accuracy $\pm 5\%$ of calibration gas value)

Gas Type	Actual Concentration	Analyzer	Gas Type	Actual Concentration	Analyzer
HC - Zero	0	-1	HC - Mid	509	527.2
HC - High	765	774	HC - Low	262	272.1

ZERO & SPAN DRIFT: (Accuracy $\pm 3\%$ of span)

Run #	Time:	
1	11:25-12:25	
Gas Type	Initial Response	Final Response
HC - Zero	-1	-1.7
HC -	527.2	526.8

Run #	Time:	
Gas Type	Initial Response	Final Response
HC - Zero		
HC -		

Run #	Time:	
2	14:25-15:25	
Gas Type	Initial Response	Final Response
HC - Zero	-1.7	0.3
HC -	526.8	527.0

Run #	Time:	
Gas Type	Initial Response	Final Response
HC - Zero		
HC -		

Run #	Time:	
3	16:33-17:33	
Gas Type	Initial Response	Final Response
HC - Zero	-50.3	-5.5
HC -	527.0	527.4

Run #	Time:	
Gas Type	Initial Response	Final Response
HC - Zero		
HC -		

INSTRUMENTAL ANALYSIS CALIBRATION DATA

DILUENT NO_x MONITORS

Plant Lehrman-Roberts

Location Memphis TN

Date 9-3-91

Operator NA

Initial Calibration (Accuracy: ± 2% Span)

Gas Type	Actual Concentration	Analyzer Response
NO _x -Zero	0.0	- .5
NO _x -High	845	848.7
NO _x -Mid	551	556.9

System Bias Response: Analyzer Response-Initial Bias = ± 5% Span
 Final Bias - Initial Bias = ± 3% Span

Run # 1 Time: 11:25-12:25

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	- .5	.2	
NO _x	556.9	551.9	

Run # 2 Time: 14:25-15:25

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	.2	.5	
NO _x	551.9	554.5	

Run # 3 Time: 16:33-17:33

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	.5	.6	
NO _x	544.5	545.2	

Run # Time:

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero			
NO _x			

INSTRUMENTAL ANALYSIS CALIBRATION DATA

DILUENT SO₂ MONITORS

Plant Lehman-Roberts

Location Memphis, TN

Date 9-3-91

Operator KA

Initial Calibration (Accuracy: ± 2% Span)

Gas Type	Actual Concentration	Analyzer Response
SO ₂ -Zero	0.0	-3
SO ₂ -High	82.8	82.3
SO ₂ -Mid	57.3	57.6

System Bias Response: Analyzer Response-Initial Bias = ± 5% Span
 Final Bias - Initial Bias = ± 3% Span

Run # 1 Time: 11:25-12:25

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	-3	-5	
SO ₂	57.6	57.4	

Run # 2 Time: 14:25-15:25

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	-5	-3	
SO ₂	57.4	57.4	

Run # 3 Time: 16:33-17:33

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	-3	-4	
SO ₂	57.4	57.3	

Run # Time:

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero			
SO ₂			

D. METHOD 5 SAMPLING EQUIPMENT

IX. CALIBRATIONS

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number 10.3-91 Date 10.3.91 Meter box number C-185 Plant _____
 Barometric pressure, $P_b = 29.99$ in. Hg Dry gas meter number 638809 Pretest Y _____

Orifice manometer setting, (ΔH), in. H ₂ O	Gas volume		Temperature			Time (θ), min	Vacuum setting, in. Hg	Y_i	Y_i
	Wet test meter (V_w), ft ³	Dry gas meter (V_d), ft ³	Wet test meter (t_w), °F	Inlet (t_{d_i}), °F	Outlet (t_{d_o}), °F				
1	10	171.1	77	106	84	95.5		1.023	$V_w P_b (t_d + 460)$ $V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)$
1	10	176.6	77	106	84	96		1.026	1.406
2	10	187.1	77	106	84	96		1.026	1.398
		202.156							1.418
									Y = 1.025
									1.407

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d where

V_w = Gas volume passing through the wet test meter, ft³.

V_d = Gas volume passing through the dry gas meter, ft³.

t_w = Temperature of the gas in the wet test meter, °F.

t_{d_i} = Temperature of the inlet gas of the dry gas meter, °F.

t_{d_o} = Temperature of the outlet gas of the dry gas meter, °F.

t_d = Average temperature of the gas in the dry gas meter, obtained by the average of t_{d_i} and t_{d_o} , °F.

ΔH = Pressure differential across orifice, in. H₂O.

Y_i = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs;
 tolerance = pretest Y \pm 0.05Y.

P_b = Barometric pressure, in. Hg.

θ = Time of calibration run, min.

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number 9-2-91 Date 9-2-91 Meter box number C-185 Plant Pretest Y
 Barometric pressure, $P_b =$ in. Hg Dry gas meter number 638809

Orifice manometer setting, (ΔH) , in. H ₂ O	Gas volume		Temperature			Time (θ) , min	Vacuum setting, in. Hg	Y_i	Y_i
	Wet test meter (V_w) , ft ³	Dry gas meter (V_d) , ft ³	Wet test meter (t_w) , °F	Inlet (t_{d_i}) , °F	Dry gas meter Average (t_d) , °F				
.5	10.5	160.7	73	98	87.5	13.66		1.014	$V_w P_b (t_d + 460)$ $V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)$
1	10	167.6	73	96	87	16.04		1.01	
2	10	179.5	73	96	87.5	11.46		1.009	
									$Y = 1.011$

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d where

V_w = Gas volume passing through the wet test meter, ft³.

V_d = Gas volume passing through the dry gas meter, ft³.

t_w = Temperature of the gas in the wet test meter, °F.

t_{d_i} = Temperature of the inlet gas of the dry gas meter, °F.

t_{d_o} = Temperature of the outlet gas of the dry gas meter, °F.

t_d = Average temperature of the gas in the dry gas meter, obtained by the average of t_{d_i} and t_{d_o} , °F.

ΔH = Pressure differential across orifice, in. H₂O.

Y_i = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest $Y \pm 0.05Y$.

P_b = Barometric pressure, in. Hg.

θ = Time of calibration run, min.

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number 7-30-91 Date 7-30-91 Meter box number C-124 Plant Pretest Y
 Barometric pressure, $P_b = 30.22$ in. Hg Dry gas meter number _____

Orifice manometer setting, (ΔH), in. H ₂ O	Gas volume		Temperature			Time (θ), min	Vacuum setting, in. Hg	Y_i	Y_i
	Wet test meter (V_w), ft ³	Dry gas meter (V_d), ft ³	Wet test meter (t_w), °F	Inlet (t_{d_i}), °F	Dry gas meter Outlet (t_{d_o}), °F				
.5	105	268 221.314	77	92 84	81 82	13.66		.954	$V_w P_b (t_d + 460)$ $V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)$ 2.062
1	10	271.5 232.037	77	90 110	84 84	19.23		.994	2.04
2	10	232.4 243.114	77	108 112	84 84	13.63		.982	2.031
								$Y = .97$	2.04

a. If there is only one thermometer on the dry gas meter, record the temperature under t_d where

V_w = Gas volume passing through the wet test meter, ft³.

V_d = Gas volume passing through the dry gas meter, ft³.

t_w = Temperature of the gas in the wet test meter, °F.

t_{d_i} = Temperature of the inlet gas of the dry gas meter, °F.

t_{d_o} = Temperature of the outlet gas of the dry gas meter, °F.

t_d = Average temperature of the gas in the dry gas meter, obtained by the average of t_{d_i} and t_{d_o} , °F.

ΔH = Pressure differential across orifice, in. H₂O.

Y_i = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs;
tolerance = pretest $Y \pm 0.05Y$.

P_b = Barometric pressure, in. Hg.

θ = Time of calibration run, min.

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number 10-13-91 Date 10-13-91 Meter box number C-124 Plant
 Barometric pressure, $P_b = 30.12$ in. Hg Dry gas meter number 44882 Pretest Y

Orifice manometer setting, (ΔH) , in. H ₂ O	Gas volume		Temperature			Time (θ) , min	Vacuum setting, in. Hg	Y_i	$V_w P_b (t_d + 460)$ $V_d \left(P_b + \frac{\Delta H}{13.6} \right) (t_w + 460)$
	Wet test meter (V_w) , ft ³	Dry gas meter (V_d) , ft ³	Wet test meter (t_w) , °F	Inlet (t_{d_i}) , °F	Dry gas meter Outlet (t_{d_o}) , °F				
1.0	10	642.44 253.15	73	108 110	84 84	19:02	5	0.975	1.55
1.5	10	642.145 220.33	73	106 110	80 82	15:32	5	0.976	1.95
2.0	10	642.037 231.037	73	102 107	77 78	13:18	5	0.981	1.92
								$Y = 0.977$	1.54

^a If there is only one thermometer on the dry gas meter, record the temperature under t_d where

V_w = Gas volume passing through the wet test meter, ft³.

V_d = Gas volume passing through the dry gas meter, ft³.

t_w = Temperature of the gas in the wet test meter, °F.

t_{d_i} = Temperature of the inlet gas of the dry gas meter, °F.

t_{d_o} = Temperature of the outlet gas of the dry gas meter, °F.

t_d = Average temperature of the gas in the dry gas meter, obtained by the average of t_{d_i} and t_{d_o} , °F.

ΔH = Pressure differential across orifice, in. H₂O.

Y_i = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest $Y \pm 0.05Y$.

P_b = Barometric pressure, in. Hg.

θ = Time of calibration run, min.

AIR PRODUCTS AND CHEMICALS, INC.
 4522 Industry Lane
 601 Business Park
 Research Triangle Park, NC 27717
 TELEPHONE (919) 331-2077
 FAX (919) 331-2074

DATE: 08/14/90
 TIME: 10:42
 PAGE: 1

 * CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
 2541 HARBOUR AVENUE
 MEMPHIS TN 38110

CUSTOMER ACCOUNT : 351
 CUSTOMER ORDER NO : 6ARY
 ORDER NO : 951-008743
 ORDER DETAIL 950 : 5

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS 2
 WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
 (SRM'S) - REFERENCE APC1 360 FIELD DIRECTIVE BOOK 1 PART A-7.

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: CARBON MONOXIDE IN NITROGEN

CIL NO	COMPONENT SEQUESTER	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE	
BATCH NO: 00102 ANAL DATE: 08/14/90	0607910	CARBON MONOXIDE NITROGEN	1000	950 BALANCE	MOLAR PER
	0668101010	CARBON MONOXIDE NITROGEN	1000	901 BALANCE	MOLAR PER

Ramcon

CERTIFICATION:

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
 ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
 ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Clyde L. Johnson

 AUTHORIZED SIGNATURE

4822 Industry Lane
LDI Business Park
Research Triangle Park, NC 27710
TELEPHONE (919) 361-2077
FAX (919) 361-2074

DATE: 07/26/90
TIME: 11:51
PAGE: 1

* CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
2541 HARBOR AVENUE
MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
CUSTOMER ORDER NO : GARY
ORDER NO : 351-041099
ORDER DETAIL SEQ : 1

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS 3
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM'S) - REFERENCE APC: 880 FIELD DIRECTIVE BOOK 1 PART A-3.

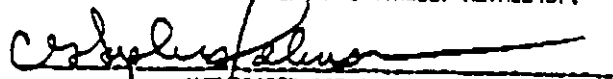
*** ANALYSIS ***

CERTIFIED GAS MIXTURE: CARBON MONOXIDE IN NITROGEN

BATCH NO	CVC NO	COMPONENT	CONCENTRATION	ANALYTICAL	UNIT OF
		REQUESTED	REQUESTED	RESULT	MEASURE
BATCH NO: 00472 ANAL DATE: 07/26/90	88880713ALB	CARBON MONOXIDE NITROGEN	300	300 BALANCE	MG/LAR PPM

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).



AUTHORIZED SIGNATURE

 * CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
 2841 HARBOR AVENUE
 MEMPHIS TN 38110

CUSTOMER ACCOUNT : 051
 CUSTOMER ORDER NO : GARY
 ORDER NO : 361-20190
 ORDER DETAIL 990 : 2

REMARKS : GAS MIXTURES LISTED BELOW ARE TRACEABLE TO NIST CLASS 3
 WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
 (SRM'S) - REFERENCE APCI 990 FIELD DIRECTIVE BOOK 1 PART A-3.

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: CARBON MONOXIDE ON NITROGEN

BATCH NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
BATCH NO: 00474 ANAL DATE: 07/28/90	368472245 CARBON MONOXIDE NITROGEN	500	596 BALANCE	MOLAR PPM

Post-It™ brand fax transmittal memo 7571 # of pages 3

To: Joel Sewel	From: Cathy
Co: Ramcon	Co: APCI-Durham
Dept:	Phone: 919-361-4645
Fax: 919-458-2868	Fax: 919-361-2074

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
 ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
 ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Cathy Sewel
 AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
 4825 Industry Lane
 690 Business Park
 Research Triangle Park, NC 27713
 TELEPHONE (919) 331-2677
 FAX (919) 331-2074

DATE: 02/26/91
 TIME: 11:51
 PAGE: 1

 * CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
 1541 HARBOR AVENUE
 MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
 CUSTOMER ORDER NO : 6ARY
 ORDER NO : 351-957503
 ORDER DETAIL SEQ : 2

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS 5
 WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
 (SRM'S) - REFERENCE APCI 990 FIELD DIRECTIVE BOOK 1 PART A-3.

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: CARBON DIOXIDE IN NITROGEN

DATE NO:	SOLICITOR	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
ANAL DATE: 02/26/91		CARBON DIOXIDE NITROGEN	17	17.0 BALANCE	WGLAR %
	0391758	CARBON DIOXIDE NITROGEN	17	17.0 BALANCE	WGLAR %

RAMCON

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
 ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
 ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Mark J. Smith

 AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
4822 Industry Lane
UDI Business Park
Research Triangle Park, NC 27713
TELEPHONE (919) 351-2077
FAX (919) 351-2074

DATE: 06/17/91
TIME: 12:01
PAGE: 1

00413

* CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
2541 HARBOR AVENUE
MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
CUSTOMER ORDER NO : 6ARY
ORDER NO : 351-084180
ORDER DETAIL SEQ : 11

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS S
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM's) - REFERENCE APCI 560 FIELD DIRECTIVE BOOK 1 PART A-3.

== ANALYSIS ==

CERTIFIED GAS MIXTURE: 2 COMPONENTS IN NITROGEN

BATCH NO:	CYL NO	COMPONENT	CONCENTRATION	ANALYTICAL	UNIT OF
		REQUESTED	REQUESTED	RESULT	MEASURE
03764	50030834B	CARBON DIOXIDE	10	10.5	MOLAR %
06/14/91		OXYGEN	10	10.2	MOLAR %
		NITROGEN		BALANCE	

RANCON

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

[Handwritten Signature]

AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
4822 Industry Lane
UDI Business Park
Research Triangle Park, NC 27713
TELEPHONE (919) 361-2077
FAX (919) 361-2074

DATE: 06/03/91
TIME: 10:49
PAGE: 1

* CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
3541 HARBER AVENUE
MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
CUSTOMER ORDER NO : 6ARY
ORDER NO : 351-063526
ORDER DETAIL SEQ : 3

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS B
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM's) - REFERENCE APCI 960 FIELD DIRECTIVE BOOK I PART A-1.

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: METHANE IN NITROGEN

	CYL NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
BATCH NO: 00543	3619815B	METHANE	850	745	MOLAR PPM
ANAL DATE: 06/03/91		NITROGEN		BALANCE	

RAMCON 6-20-91

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS /THESE/ METHOD(S).

[Signature]

AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
 1822 Industry Lane
 UDC Business Park
 Research Triangle Park, NC 27713
 TELEPHONE (919) 351-2077
 FAX (919) 351-2074

DATE: 06/03/91
 TIME: 10:49
 PAGE: 1

 * CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
 2541 HARBOUR AVENUE
 MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
 CUSTOMER ORDER NO : GARY
 ORDER NO : 351-063536
 ORDER DETAIL SEQ : 1

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS B
 WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
 (GRM'S) - REFERENCE APO: SSD FIELD DIRECTIVE BOOK I PART A-3.

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: METHANE IN NITROGEN

BATCH NO:	CYL NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
03642	SG00FF92B	METHANE	350	282	MOLAR FPN
ANAL DATE: 06/03/91		NITROGEN		BALANCE	

RAMCON 6-20-91

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
 ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
 ANALYTICAL ACCURACIES OF THIS METHOD(S).

Steve Rutledge

 AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
1622 Industry Lane
UBI Business Park
Research Triangle Park, NC 27713
TELEPHONE (919) 361-2077
FAX (919) 361-2074

TIME: 10:48
PAGE: 1

: CERTIFICATE OF ANALYSIS :

AIR PRODUCTS AND CHEMICALS, INC.
2541 HARBOR AVENUE
MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
CUSTOMER ORDER NO : GARY
ORDER NO : 351-063526
ORDER DETAIL SEQ : 2

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS B
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS
(SRM'S) - REFERENCE APO: 960 FIELD DIRECTIVE BOOK I PART A-3.

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: METHANE IN NITROGEN

BATCH NO:	CYL NO	COMPONENT	CONCENTRATION	ANALYTICAL	UNIT OF
		REQUESTED	REQUESTED	RESULT	MEASURE
00641	56119528	METHANE	500	509	MOLAR PPM
ANAL DATE: 06/05/91		NITROGEN		BALANCE	

RAMCON 6-20-91

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

[Signature]

AUTHORIZED SIGNATURE

4822 Industry Lane
LDI Business Park
Research Triangle Park, NC 27712
TELEPHONE (919) 361-2077
FAX (919) 361-2074

TIME: 10:50
PAGE: 1

* CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
3941 HARBOR AVENUE
EMERYVILLE OH 44013

CUSTOMER ACCOUNT : 731
CUSTOMER ORDER NO : 3491
ORDER NO : 351-042571
ORDER DETAIL SEQ : 2

*** ANALYSIS IS

CERTIFIED GAS MIXTURE: NITROGEN DIOXIDE IN NITROGEN		CONCENTRATION	ANALYTICAL	UNIT OF
WT. %	COMPONENT	PERCENT	RESULT	MEASURE
BATCH NO: 00684	NITROGEN DIOXIDE	500	545	MLAR PER
ANAL DATE: 08/22/90	Nitrogen Dioxide		3.5	MLAR PER
	NITROGEN		BALANCE	

CERTIFICATION

THIS ANALYSIS WAS OBTAINED UTILIZING A VOLUMETRIC ANALYTICAL METHOD AND IS CORRECT TO WITHIN THE ANALYTICAL ACCURACIES OF THIS (CLASS) METHOD (S).



AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
 4832 Industry Lane
 UDI Business Park
 Research Triangle Park, NC 27713
 TELEPHONE (919) 361-2077
 FAX (919) 361-2074

DATE: 08/24/90
 TIME: 14:53
 PAGE: 1

 * CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
 2541 HARBOR AVENUE
 MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
 CUSTOMER ORDER NO : BARY
 ORDER NO : 351-042705
 ORDER DETAIL 352 : 4

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: NITRIC OXIDE IN NITROGEN

CYL NO	COMPONENT REQUESTED	CONCENTRATION		ANALYTICAL RESULT	UNIT OF MEASURE
		REQUESTED	FOUND		
BATCH NO: 00935 ANAL DATE: 08/24/90	60700644LB NITRIC OXIDE Nitrogen Dioxide NITROGEN	350	351	3 BALANCE	MOLES PER MOLES PER

3.5% Nitrogen Dioxide in Nitrogen
2.0% Hydrogen Sulfide

49
 CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

Asst. Lab. Manager

 AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
4820 Industrial Lane
MDI Business Park
Research Triangle Park, NC 27710
TELEPHONE (919) 351-2077
FAX (919) 351-2074

DATE: 02/15/91
TIME: 13:00
PAGE: 1

* CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
3541 HARBOUR AVENUE
MEMPHIS TN 38117

CUSTOMER ACCOUNT : 051
CUSTOMER ORDER NO : 0474
ORDER NO : 051-000009
ORDER DETAIL EED : 0

ANALYSIS IS

CERTIFIED GAS MIXTURE: SULFUR DIOXIDE (S) NITROGEN

	SYL NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
BATCH NO:	00580	SOPACIDIALB	05	90.9	MOLAR FEM
ANAL DATE:	02/11/91	SULFUR DIOXIDE NITROGEN		BALANCE	

RAMCON

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED ANALYTICAL METHODS AND IS CORRECT TO WITHIN THE ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

[Signature]

AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.
4822 Industry Lane
UDI Business Park
Research Triangle Park, NC 27713
TELEPHONE (919) 361-2077
FAX (919) 361-2074

DATE: 04/10/91
TIME: 12:04
PAGE: 1

* CERTIFICATE OF ANALYSIS *

AIR PRODUCTS AND CHEMICALS, INC.
2541 HARBOR AVENUE
MEMPHIS TN 38113

CUSTOMER ACCOUNT : 351
CUSTOMER ORDER NO : GARY
ORDER NO : 351-059075
ORDER DETAIL SEQ : 1

*** ANALYSIS ***

CERTIFIED GAS MIXTURE: SULFUR DIOXIDE IN NITROGEN

	CYL NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
BATCH NO: 03126 ANAL DATE: 04/03/91	561123NB	SULFUR DIOXIDE NITROGEN	55	57.3 BALANCE	MOLAR PPM

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).



AUTHORIZED SIGNATURE

Name: Mr. G. Sumner Buck, III
Title: President

Qualifications:

Mr. Buck is a graduate of the University of Mississippi with graduate studies at Memphis State University and State Technical Institute of Memphis. He is a graduate of the EPA 450 "Source Sampling for Particulate Pollutant's" course and the 474 "Continuous Emissions Monitoring" courses outlined by EPA at Research Triangle Park, N.C. He has been directly involved in conducting and supervising air emission testing for over 15 years. He has personally conducted over 400 air emission tests. He currently sponsors and directs visual emission certification schools for US EPA Method 9.

Project Duties:

Mr. Buck will be responsible for the overall supervision of the project. He provided supervision for the project preparation, testing schedules for each team on-site, and overall organization between the testing crews and facility.

Name: Mr. Ken Allmendinger
Title: Field Supervisor

Qualifications:

Mr. Allmendinger is currently our Field Supervisor. He provides leadership to other Team Leaders when projects require multiple teams on site as well as coordinating with plant personnel. He has been employed with RAMCON Environmental Corporation for over six years. During that time he has personally conducted over 500 air emission tests. He has extensive training in conducting both isokinetic and instrumental US EPA Reference Methods. He has a current V.E. certification to conduct Method 9 for opacity. He has attended several equipment manufacturers schools for further knowledge of the processes he is testing.

Project Duties:

Mr. Allmendinger provided project leadership at the facility. He provided on-site organization for each Team Leader as to his crews responsibilities as well as providing coordination of testing time periods with the plant personnel.

Name: Mr. Ray Jenkins
Title: Team Leader - Instrumental

Qualifications:

Mr. Jenkins is the Team Leader for our gas chromatography sampling team. He is a graduate of Memphis State University where he obtained a bachelor of science degree with a major emphasis in chemistry. He also serves as a laboratory technician for various specialized analysis procedures conducted in our laboratory. He has experience in conducting the full scope of isokinetic test methods, however he specializes in portable gas chromatography instrumentation methodology. He currently is certified to conduct Method 9 for opacity.

Project Duties:

Mr. Jenkins served as the Team Leader for the testing procedures. He was responsible for conducting the calibration and operation of the gas chromatograph.

Name: Mr. Joe Sewell
Title: Instrumentation Director

Qualifications:

Mr. Sewell is the director of our instrumental analysis branch of air emissions testing. He is a graduate of Christian Brothers University in Memphis, Tennessee where he obtained a bachelor of science degree in Chemical Engineering. He has personally conducted and supervised air emissions testing of boilers, incinerators, refineries, etc. utilizing state of the art continuous instrumentation and gas chromatography. He is learned in all US EPA methods with expertise in instrumental techniques for conducting compliance tests and Performance Specifications for CEMS certifications.

Project Duties:

Mr. Sewell provided project leadership for all test procedures conducted at the facility. He is the Quality Assurance/Quality Control Coordinator and will provided guidance in QA/QC to each team leader with regard to individual responsibilities on site for all testing procedures. He acted as a secondary contact person for RAMCON Environmental Corporation.

Name: Mr. Bill Lockett
Title: Team Leader

Qualifications:

Mr. Lockett has been employed by RAMCON Environmental Corp. for three years. He has recently completed Team Leader training in isokinetic and proportional test methods. He currently is certified in conducting Method 9 for opacity. He has been involved in conducting tests on process stacks, incinerators, boilers, etc. He has served as a Field Technician for over two years, however he has recently been upgraded to Team Leader.

Project Duties:

Mr. Lockett is responsible for conducting isokinetic sampling procedures at the facility(s). He is responsible for preparation, calibration and cleaning of the necessary equipment for this testing. His duties on-site include assembling the sample train, leak checking the system, operation of the train and recording the test data on the field data forms.

Name: Mr. Tim Huey
Title: Laboratory Technician

Qualifications:

Mr. Huey is currently serving as Laboratory Technician. He is proficient in conducting many analysis procedures such as front and back-half particulate analysis, titrations, extractions, etc. He received an associate degree in Chemical Engineering from State Technical Institute in Memphis.

Project Duties:

Mr. Huey conducts the laboratory analysis on the particulate samples. He is also responsible for accepting the remaining field samples from the Field Sample Bank Manager and performing inspection as to integrity. He documents the transfer on the chain of custody forms and distributed the subcontracted samples to the respective laboratories.

Name: Mr. Charles Crook
Title: Team Leader

Qualifications:

Mr. Crook has been employed by RAMCON Environmental Corp. for three years. He has recently completed Team Leader training in isokinetic and proportional test methods. He currently is certified in conducting Method 9 for opacity. He has been involved in conducting tests on process stacks, incinerators, boilers, etc. He has served as a Field Technician for over two years, however he has recently been upgraded to Team Leader.

Project Duties:

Mr. Crook is responsible for conducting isokinetic sampling procedures at the facility(s). He is responsible for preparation, calibration and cleaning of the necessary equipment for this testing. His duties on-site include assembling the sample train, leak checking the system, operation of the train and recording the test data on the field data forms.