

POST-SEAL INTERNATIONAL, INC.

North Stonington, CT 06350

LOCA & SEISMIC ANALYSIS

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UNIT: Nine Mile Point Nuclear  
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- ENCLOSURE
- (1) Valve Assembly Dwgs 19157-3 Rev. B  
19157-4 Rev. A  
19157-5 Rev. C
  - (2) Posi-Seal Technical Bulletin No. 2,  
dated June 1982
  - (3) Derivation of Hydrodynamic Torque Curves
  - (4) Posi-Seal Technical Bulletin No. 1A,  
dated June 1982

- REFERENCES
- (a) DuPont Tefzel Catalog, A-95151, dated 1973
  - (b) "Flow of Fluids through Valves, Fittings  
and Pipe", Technical Paper No. 410, Crane
  - (c) Nuclear Seismic Analysis 19157SQ-01, Rev. A  
dated July 18, 1983
  - (d) Stone & Webster Letter No. 9M2-15,128  
dated December 13, 1983
  - (e) Stone & Webster Dwg 12177-EB-15AJ-9
  - (f) Stone & Webster Dwg 12177-EB-15N-10
  - (g) Stone & Webster Dwg 12177-EB-15P-9
  - (h) Stone & Webster Dwg 12177-EB-15F-9
  - (i) Stone & Webster Dwg 12177-EB-156-8



SUMMARY

Due to the design of the Posi-Seal butterfly valve with the disc being asymmetrical, flow in the preferred direction tends to close the valve. In the nonpreferred direction the disc tends to stay in the open position until it reaches an angle of approximately 75 degrees open, then tends to close. The preferred direction is with the stem side of the disc upstream and the retaining ring downstream. See Figure 1 on Page 2.

For the purpose of this report the orientation of the valves relative to the flow will be based on the flow going from containment to outside containment.

If a Loss of Coolant Accident (LOCA) does occur, the scenario given below describes what effect the large flows resulting from the LOCA will have on the subject valves.

A. If all the subject valves are fully open

1. Valves AOV 106, 108 and 109 which are inside containment and are presently installed in the preferred direction.

Due to the large flow resulting from the LOCA and the corresponding aerodynamic torque, these valves will partially close. Upon receiving a signal to close, these valves will fully close providing proper shut-off.

2. Valve AOV 107, which is inside the containment and presently installed in the nonpreferred direction.

Upon receiving a signal to close, this valve will fully close and provide proper shut-off.



3. Valves AOV 104, 110 and 111 which are outside containment and are presently installed in the nonpreferred direction.

The aerodynamic torques resulting from a LOCA event will be so large that the Bettis actuators will not be able to overcome the torque. As a consequence, these valves will remain in the open position until which time the pressure inside containment reduces to a point where the resulting torque is less than that of the actuator.

- b. Valve AOV 105 which is outside containment and presently installed in the nonpreferred direction.

Upon receiving the signal, this valve will close, however, the closing time will exceed the 5 second requirement.

- B. If the recommendations made in this report are incorporated -

Upon receiving the closing signal all the valves will full close providing a proper shut off.

Preferred Direction

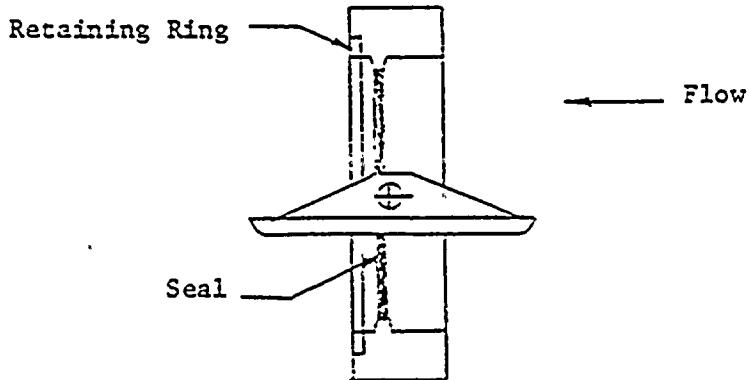


Figure 1



INTRODUCTION

The objective of this analysis is to show that the subject containment isolation valves can withstand a Loss of Coolant Accident (LOCA) as well as a seismic event of magnitude as given in customer's specification and still maintain operability.

The escape of containment atmosphere during a LOCA will result in aerodynamic torques acting on the valve assembly if it is in the open position. These torques are a result of the disc acting like an airfoil wanting to rotate about the axis of the stem. This analysis will determine the magnitude of the aerodynamic torque and its effect on the operation of the valve assembly.

The seismic aspect of the analysis will consist of determining the natural frequencies and stresses of the valve assembly, assuming the basic valve body to be rigid and the actuator to act as a lumped mass concentrated at its C.G. and rigidly connected to the valve bracket through the bracket bolting.

Those critical sections of the valve assembly such as the bolting, neck, stem and pin are analyzed assuming a g static load (magnitude per customer specification) applied at either actuator or disc C.G., in each of the orthogonal directions simultaneously. Seismic stresses are combined with operating stresses as well as the stresses due to the LOCA aerodynamic torque.

Section modulus of the valve body and deflection of the actuator relative to the valve due to seismic loading are also analyzed.



The valves to be qualified by this analysis are as follows:

<u>PSI Item No.</u>	<u>Description</u>	<u>Tag No.</u>
19157-3	14"-150 Cl with Bettis N721C-SR80-M3HW	ACV104 AOV106 AOV108 AOV110
-4	12"-150 Cl with Bettis N721C-SR80-M3HW	AOV107 AOV109
-5	12"-150 Cl with Bettis N721C-SR80-M3HW	AOV105 ACV111

The assembly drawings of these valves are shown in Enclosure (1).



RESULTS

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Maximum Torques Resulting from a LOCA  
and Closing Times

Tag No.	AOV106	AOV104	AOV108	AOV110
SL Item No.	3	3	3	3
Base No.	1A	1B	2A	2B
Valve Size	14"	14"	14"	14"
lettis Actuator Model	N721C-SR80	N721C-SR80	N721C-SR80	N721C-SR80
Actuator Max Allow Torque	22,500	22,500	22,500	22,500
Max Torque Resulting from a LOCA (In.lbs)				
Preferred Direction				
80°	6170	6519	5848	9584
70° Max Opening	-	-	-	-
Nonpreferred Direction				
90°	-	7339	-	7287
70° Max Opening	-	3101 (Seating Torque)	-	3101 (Seating Torque)
Calculated				
Closing Times (Sec.)				
No Flow	1.5	1.5	1.5	1.5
Preferred Direction				
Valve Opened to 90°	.8	1.00	.8	.6
Valve Opened to 70°	-	-	-	-
Nonpreferred Direction				
Valve Opened to 90°	-	Will Not Close	-	Will Not Close
Valve Opened to 70°	-	1.4	-	2.6
Required Closing Time	5.0	5.0	5.0	5.0



RESULTS

Maximum Torques Resulting from a LOCA  
and Closing Times

Tag No.	AOV107	AOV105	AOV109	AOV111
PSI Item No.	4	5	4	5
Case No.	3A	3B	4A	4B
Valve Size	12"	12"	12"	12"
Bettis Actuator Model	N721C-SR80	N721C-SR80	N721C-SR80	N721C-SR80
Actuator Max Allow Torque	22,500	22,500	22,500	22,500
Max Torque Resulting from a LOCA (in.lbs)				
Preferred Direction				
80°	3237	4100	3330	6776
70° Max Opening	-	-	-	4729
Nonpreferred Direction				
90°	3998	4485	-	5174
70° Max Opening	2542 (Seating Torque)	2542 (Seating Torque)	-	2542 (Seating Torque)
Calculated Closing Times (Sec.)				
No Flow	1.5	1.5	1.5	1.5
Preferred Direction				
Valve Opened to 90°	.75	1.15	.8	.85
Valve Opened to 70°	-	-	-	.65
Nonpreferred Direction				
Valve Opened to 90°	3.9	5.75	-	Will Not Close
Valve Opened to 70°	1.5	1.5	-	2.1
Required Closing Time	5.0	5.0	5.0	5.0



RESULTSLOCA AND SEISMIC STRESSES (PSI)33375SL-001Page - 7

Tag No.	Size	Valve Opening	Flow Direction	Actuator Bolt		Bracket Bolt		Bracket		Valve Neck		Stem		Disc Pin	
				Calc	Allow	Calc	Allow	Calc	Allow	Calc	Allow	Calc	Allow	Calc	Allow
AOV106	14"	80°	Preferred	15019	37500	20400	37500	3765	18900	1722	23400	14522	52800	14808	31680
AOV104	14"	90°	Non-Preferred	17018	37500	21557	37500	3983	18900	1805	23400	16761	52800	17614	31680
AOV108	14"	80°	Preferred	14788	37500	20255	37500	3701	18900	1705	23400	13902	52800	14035	31680
AOV110	14"	80°	Preferred	18168	37500	24240	37500	5105	18900	2166	23400	21138	52800	23002	31680
AOV107	12"	90°	Non-Preferred	14795	37500	21162	37500	3313	18900	9640	23400	13005	52800	22977	31680
AOV105	12"	90°	Non-Preferred	15107	37500	25495	37500	3443	18900	31.78	23400	14258	52800	25776	31680
AOV109	12"	80°	Preferred	14376	37500	20817	37500	3179	18900	9551	23400	11297	52800	19138	31680
AOV111	12"	80°	Preferred	16632	37500	26431	37500	3903	18900	3376	23400	20203	52800	38943	31680
		70°	Preferred	15265	37500	25590	37500	3492	18900	31.98	23400	14888	52800	27178	31680

NOTE: The allowable stresses are based on 1.5 times the allowable given in Section III of the ASME Boiler and Pressure Vessel Code



RECOMMENDATIONS AND CONCLUSIONS

Based on the results of this analysis, Posi-Seal recommends that all the subject valves be installed in the preferred direction and that the amount of valve open of valve AOV111 be restricted to 70 degrees. For valves inside containment the retaining ring will be on the side of the valve closest to the containment wall. For the valves outside containment the retaining ring will be on the side the farthest from the containment wall. Valves AOV110 and AOV111 should be orientated as shown on Pages 31 and 33, respectively.

If, for some reason a valve cannot be installed in the preferred direction, then the amount of valve opening should be restricted to 70 degrees.

Posi-Seal recommends that one of the two methods shown on the following page be used to restrict the amount of valve opening.

It is concluded that if the above recommendations are incorporated the subject valves will properly operate within the required time during a combined LOCA and seismic event. Whether the amount of pressure drop across the valves under normal flow conditions is acceptable with the amount of valve opening restricted to 70 degrees remains for Stone & Webster to determine. See Page H-1 in Appendix H.

The ability of the Tefzel seals to provide a proper shut off is based on the following:

1. Posi-Seal's experience with Tefzel seals in applications where the velocities are comparable to those the subject valves will experience during a LOCA.
2. Radiation testing performed by DuPont as reported in Reference (a). For Posi-Seal's application we have rated the Tefzel seals to  $3 \times 10^8$  rads.
3. The ability of Tefzel to withstand 340 degrees F. temperatures for a short period of time as also reported in Reference (a).



BETTIS ACTUATOR  
Mechanical Stops for  
Restricting Valve Opening to 70°

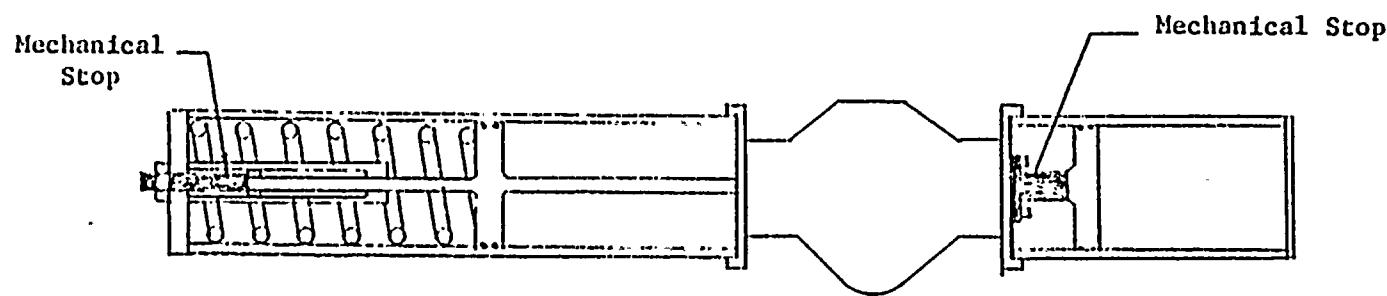


Figure 1



LOCA ANALYSIS

The purpose of this analysis is to determine what effects the aerodynamic torque resulting from a LOCA will have on a valve assembly. Since aerodynamic torque is dependent upon the flow conditions and the valve angle, computer programs are developed which:

1. Models the piping system
2. Determines the flow at various valve angles
3. Simulates the actuator as it strokes the valve from fully open to fully close.

MODELING THE PIPING SYSTEM

For the subject crder there are four piping systems which are to be investigated. They are:

Case 1 A 14" Valve AOV106 Cycles Close  
B 14" Valve AOV104 Cycles Close

Case 2 A 14" Valve AOV108 Cycles Close  
B 14" Valve AOV110 Cycles Close

Case 3 A 12" Valve AOV107 Cycles Close  
B 12" Valve AOV105 Cycles Close

Case 4 A 12" Valve AOV109 Cycles Close  
B 12" Valve AOV111 Cycles Close

Shown in Appendix A are schematics of the piping systems with each system broken down into the individual components with its corresponding resistance factor. These factors are inputted into the computer program either as a K value, as a length of pipe, a change in pipe diameter, or as a valve C. The K values are obtained from Reference (b), the C<sub>v</sub> values from Posi-Seal Technical Bulletin No. 2, Enclosure (2).



Thus, with the piping system modeled, and with the upstream and downstream conditions known, the flow conditions can be determined.

### Determination of Flow Conditions

Derivation of equations

Bernoulli's Equation

$$z_1 + \frac{144 p_1}{\rho_1} + \frac{v_1^2}{2g} = z_2 + \frac{144 p_2}{\rho_2} + \frac{v_2^2}{2g} + h_L$$

Since the flow investigated will either be steam or air the height terms ( $z_1$ ,  $z_2$ ) can be ignored.

$$\frac{144 p_1}{\rho_1} + \frac{v_1^2}{2g} = \frac{144 p_2}{\rho_2} + \frac{v_2^2}{2g}$$

where  $P$  = Pressure PSIG

$\rho$  = Density lb/ft<sup>3</sup>

$V$  = Velocity ft/sec

$g$  = Gravitational constant = 32.2 ft/sec<sup>2</sup>

$h_L$  = Head Loss

Since the piping systems are relatively short the flow is assumed to be adiabatic.

$$\rho_2 = \rho_1 \left( \frac{P_2'}{P_1'} \right)^{1/K_1} \quad \text{per Ref. (b)}$$

$$T_2 = T_1 \left( \frac{P_2'}{P_1'} \right)^{\frac{K_1 - 1}{K_1}}$$



where  $\gamma_1$  = Ratio of specific heats  
 $P'$  = Pressure PSIA  
 $T$  = Absolute temperature °R

### Flow equations

#### In pipe

$$Q = \frac{694.3 P' v D^2}{T}$$

where  $Q$  = Flow SCFH  
 $D$  = Diameter in<sup>2</sup>

#### In valve

$$Q = 1360 C_v P_1' Y \sqrt{\frac{X}{GTZ}} \quad \text{per Encl. (2)}$$

where  $C_v$  = Valve coefficient

$$X = \Delta P/P'$$

$\Delta P$  = Pressure drop across valve PSI

$$Y = 1 - \frac{X}{3F_K X_T}$$

$F_K$  = Ratio of specific heat factors

$X_T$  = Rated pressure drop ratio factor

$G$  = Specific gravity

$Z$  = Compressibility factor

#### For choke flow in valve

$$Q = 907.1 C_v P_1' \sqrt{\frac{F_K X_T}{G T Z}} \quad \text{per Encl. (2)}$$

$$\Delta P_{\text{choked}} = F_K X_T P_1'$$



## Sonic Velocity Equation

$$v_s = \sqrt{\frac{4637 K_1 P'}{\rho}} \quad \text{per Ref. (b)}$$

Determination of the flow conditions will be performed as follows:

1. Calculate density at the end condition

$$\rho_{N+1} = \left( \frac{P'_{N+1}}{P'_N} \right)^{\frac{1}{K_1}} \rho_1$$

2. Calculate initial velocity based on beginning and end conditions.

$$V(1) = \sqrt{\frac{\left( \frac{P_N + 1}{\rho_{N+1}} - \frac{P_1}{\rho_1} \right) 288g}{\left( 1 - \left( \frac{D_1}{D_{N+1}} \right)^{\frac{1}{K_1}} - K \right)}}$$

$$\text{where } K = K(1) + K(2) + \dots + K(N+1)$$

3. Using the initial velocity  $V(1)$ , calculate  $\Delta P$  for all the stations as shown below

For  $I = 1$  to  $N$

$$\rho = \rho(I)$$

$$\rho(I+1) = \rho$$

$$V(I+1) = D(I)^2 V(I) \rho(I) / D(I+1)^2 / \rho(I+1)$$

$$P(I) = P(I) - 14.7$$

$$P(I+1) = \rho(I+1) \left( \frac{P(I)}{\rho(I)} + \frac{V(I)^2}{9274} (1 - K(I)) \right) - \frac{V(I+1)^2}{9274}$$

$$P(I) = P(I) + 14.7 \quad P(I+1) = P(I+1) + 14.7$$

$$\rho(I+1) = \rho(I) \left( \frac{P(I+1)}{P(I)} \right)^{1/K_1}$$

$$\text{If } |\rho(I+1) - \rho| > .0005 \text{ then } \rho = \rho - .0005$$

and recalculate  $P(I+1)$

Note: This is done since  $\rho(I+1)$  is a function of  $P(I+1)$  and vice versa.

$$T(I+1) = T(I) \left( \frac{P(I+1)}{P(I)} \right) (K_1 - 1) / K_1$$



For determining the  $\Delta P$  across the valves, the equation for  $Q$ , given on the preceding page is used. Solving for  $\Delta P$  from this equation results in a cubic equation with the smallest root being equal to the actual drop across the valve.

4. With the final pressure  $P(N+1)$  calculated, this pressure is compared to the final pressure given. For this particular study the final pressure is atmospheric.

If the calculate pressure is less than the given final pressure then the initial velocity is decreased and Step 3 is repeated. The initial velocity is increased if the calculated final pressure is greater than the given final pressure.

5. Steps 3 and 4 are repeated until the calculated final pressure approximately equals the given final pressure.
6. If sonic velocity is encountered at any of the stations the initial velocity is decreased until Step 5 is achieved or until the calculated sonic velocity approximately equals the actual sonic velocity.  
If the latter is the case then the given final pressure is assumed and the pressures at the stations between the outlet and the station at which sonic flow occurs are determined by using the equation given in Step 3 in reverse order and using the flow,  $Q$ , based on the sonic velocity.
7. If choke flow is encountered in any of the valves then the same approach is taken as given in Step 6.
8. To determine the flow conditions for the various valve angles, the  $C_v$  of the valve closing is determined for the angle of interest and Steps 1 thru 7 are repeated.

The above is formulated into the computer program "FLOW-GAS."



Simulation of the Actuator Stroking the Valve Close

In order to simulate the closing of the valve, an equation which describes the torques acting on the valve stem has to be defined. This equation is given below:

$$T_{TTO} = T_{flow} + T_{air} + T_{spring} + T_{packing \text{ and seal}} + T_{bearing}$$

Where  $T_{TTO}$  = The net torque tending to open the valve (equals zero when the valve starts to close).

$T_{flow}$  = The torque due to aerodynamic flow caused by the LOCA.

$T_{air}$  = The torque exerted by the actuator as a result of the air acting on the actuator piston tending to open the valve.

$T_{spring}$  = The torque exerted by the actuator spring tending to close the valve.

$T_{packing \text{ & seal}}$  = Torque of the packing and the seal resisting the closing motion of the valve. The seal torque does not take affect until the disc begins to seal which occurs at approximately 3° from fully closed. The running torque of the packing is approximately .6 times the break away torque.

$T_{bearing}$  = Torque due to the  $\Delta P$  acting across the valve which forces the stem/disc assembly into the bearings.



p



Derivation of Torque EquationsAerodynamic Torque ( $T_{flow}$ )

Since Posi-Seal has only determined hydrodynamic torques for water based on testing, see Encl. (3), a way to determining aerodynamic torques for air and steam from those for water has to be derived.

The resultant drag and lift forces acting on the disc are as follows:

$$F_D = C_D \rho \frac{V^2 A}{2} \quad \text{Resultant Drag Force}$$

$$F_L = C_L \rho \frac{V^2 A}{2} \quad \text{Resultant Lift Force}$$

The resultant torque is the resultant force times the length from  $\xi$  of stem to the location of the resultant force.

$$\therefore T_D = C_D L_D \rho \frac{V^2 A}{2} \quad \text{Resultant Drag Torque}$$

$$T_L = C_L L_L \rho \frac{V^2 A}{2} \quad \text{Resultant Lift Torque}$$

$$T_{D,L} = C_{D,L} L_{D,L} \rho \frac{V^2 A}{2}$$

Where  $V$  = Velocity

$A$  = Surface Area

$\rho$  = Density of Fluid

$C_D$ ,  $C_L$  = Drag and Lift Coefficients (Dependent upon shape and orientation of disc)

$L_D$ ,  $L_L$  = Length  $\xi$  of stem to resultant lift and drag forces

$D,L$  = Combined Subscript



NOTE:  $C_{D,L}$  and  $L_{D,L}$  are the same for the same size and class valve, assuming the same angular position, regardless of fluid, flow, media or temperature.

$$\therefore \frac{T_{\text{fluid}}}{T_{\text{water}}} \approx \frac{\rho_{\text{fluid}} v_{\text{fluid}}^2}{\rho_{\text{water}} v_{\text{water}}^2}$$

$$T_{4F} = \rho_F \frac{T_{4W} v_F^2}{62.4 v_W^2}$$

Where W = Water

F = Fluid

$\rho_{\text{water}} = 62.4 \text{ lbs/ft}^3$

$v_F$  = Calculated in the determination of the flow conditions

$$v_W = .00223 \frac{Q}{A} = .00223 \frac{C_V}{A} \sqrt{\Delta P}$$

$T_{4W}$  = Disc Hydrodynamic Torque per PSI  $\Delta P$  (function of valve angle)

$T_{4F}$  = Disc Aerodynamic Torque per PSI  $\Delta P$

The total aerodynamic torque equals

$$T_F = \int_F \frac{T_{4W} v_F^2}{62.4 v_W^2} \Delta P$$



$$\text{Since } \rho_F = \frac{144 P_1}{R T_1} \quad \rho_{\text{Air}} = 53.34$$

$$v_F = \frac{Q T_1}{127300 P_1 A} \quad \rho_{\text{Steam}} = 65.76$$

$$V_w = .00223 C_v \sqrt{\frac{\Delta P}{A}}$$

$$\text{Then } T_F = \frac{144 P_1}{R T_1} \left( \frac{T_{4W}}{62.4} \right) \left( \frac{Q T_1}{127300 P_1 A} \right)^2 \Delta P$$

$$T_{\text{Air}} = .04326 T_{4W} \frac{T_1}{P_1} \left( \frac{g}{203.0 C_v} \right)^2$$

$$T_{\text{Steam}} = .0269 T_{4W} \frac{T_1}{P_1} \left( \frac{g}{203.0 C_v} \right)^2$$

Values for  $C_v$  and  $T_{4W}$  can be found in Enclosures (2) and (4) respectively for various valve angles.

For critical flow the equations can be simplified to:

$$T_{\text{Air}} = .441 T_{4W} \frac{F_K X_T P_1}{G Z}$$

$$T_{\text{Steam}} = .274 T_{4W} \frac{F_K X_T P_1}{G Z}$$

The above aerodynamic torque equations have also been incorporated into "FLOW-GAS" computer program such that the torque resulting from a LOCA can be determined for every 10° of valve closure.

In performing the LOCA analysis it is assumed that the valves close individually. This assumption is made for two reasons. The first is for ease of analysis. The second reason being, this is considered to be more conservative since if both valves close simultaneously the resistance in the system will be greater; consequently, the flow will be less and the aerodynamic torque will be less.



Pneumatic Torque ( $T_{air}$ )

$$T_{air} = \frac{A \cdot R \cdot P_1}{C_2}$$

Where  $A$  = Area of piston

$D_c$  = Cubic Displacement

$$A = \frac{D_c}{2R}$$

$P$  = Working Pressure of Actuator

$$A = \frac{1728}{2R} V \left( \frac{14.7}{P+14.7} \right)$$

$V$  = Specific Volume - SCF

$R$  = Radius of Scotch Yoke (See Figure 4)

$P_1$  = Pressure of the air in the piston cylinder

$$= \frac{P_1 (V - \Delta V)}{V}$$

$P_1$  = Previous pressure (See Note Below)

$\Delta V$  = Change in Volume

$$= \frac{dt \cdot Q}{3600}$$

$dt$  = Change in Time

$Q$  = Flow thru solenoid valve or quick exhaust

$$= \frac{963 C_{vs} F_{LS} P_1 \sqrt{1 - .25 (F_L)^2}}{\sqrt{GT}}$$

$C_{vs}$  =  $C_v$  of solenoid valve or quick exhaust

$F_{LS}$  = Rated liquid pressure recovery factor of a solenoid valve or quick exhaust = .9

$G$  = Specific Gravity of Air = 1

$T$  = Temperature ° Rankine = Assume equals 530°

$$Q = 33.62 C_v P_1$$

$C_2$  = Equation describing the advantage of the Scotch yoke as a function of angle.

NOTE: In order to take the effect of the building atmospheric pressure into consideration the initial pressure for  $P_1$  is equal to the working pressure of the actuator minus the building atmospheric pressure.



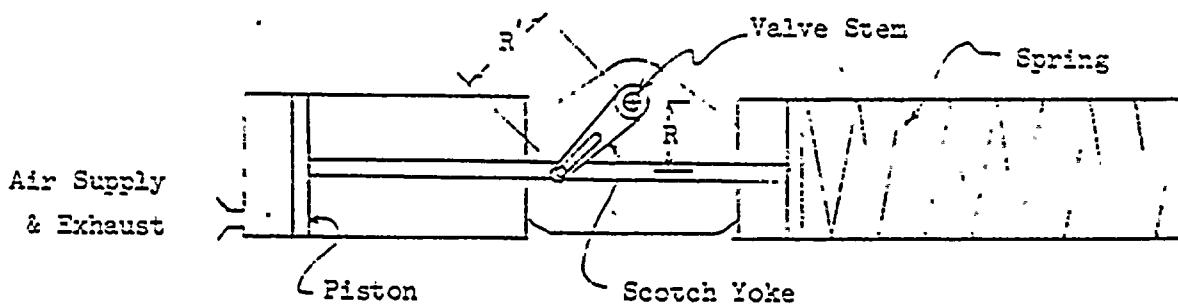


Figure 4

## Forces acting on Scotch Yoke Pin

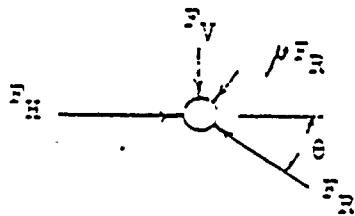


Figure 5

Summing forces in the horizontal direction

$$F_H - \cos \theta F_R - \mu \sin \theta F_R = 0$$

$$F_R = F_H / (\cos \theta + \mu \sin \theta)$$

 $F_R$  = Resultant Force $F_H$  = Horizontal Force

$$T_R = F_R R = \frac{F_R R}{\cos \theta} = \text{Resultant Torque}$$

$$\therefore T_R = \frac{T}{\cos \theta (\cos \theta + \mu \sin \theta)}$$

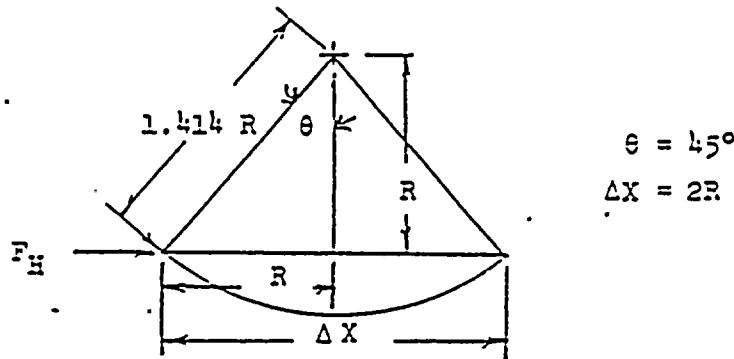
$$C2 = \cos \theta (\cos \theta + \mu \sin \theta)$$



Spring Torque ( $T_{\text{spring}}$ )

$$T_{\text{spring}} = \frac{K X_2 R}{C}$$

Figure 6



K = Spring rate

$$= \frac{\Delta F}{\Delta X} = \frac{T_{\text{spring beginning}} - T_{\text{spring ending}}}{1.414 (1.414)R} \frac{1.414 (1.414)R}{\Delta X}$$

$$K = \frac{T_{\text{spring beginning}} - T_{\text{spring ending}}}{4R^2}$$

$$X_2 = X_1 + R (1 + \tan \theta)$$

$$X_1 = \frac{T_{\text{spring ending}} C_2 \theta \epsilon}{KR}$$

$$X_1 = \frac{.571 T_{\text{spring ending}}}{KR}$$

$$X_2 = \frac{.571 T_{\text{spring ending}}}{KR} + R (1 + \tan \theta)$$

Bearing Torque ( $T_{\text{bearing}}$ )

$$T_{\text{bearing}} = \frac{\pi \mu^2 D^2 d}{8}$$

where  $\mu$  = Coefficient of friction  
= .059 for bronze bearings  
D = Disc gage diameter  
d = Stem diameter



The torque equations are formulated into the computer program "FLOW-CL". This program calculates the various torques acting on the valve and the amount of valve closure as time is incremented until which time the valve is fully closed. In order to determine the aerodynamic torque for angles other than the ten degree increments calculated by "FLOW-GAS" the values for the densities, pressure drops and velocities are taken from "FLOW-GAS", interpolated to correspond to the angle of interest and then the aerodynamic torques are calculated based on those values. The reason for calculating aerodynamic torque in this manner is that density, pressure drop and velocity are more linear between the ten degree increments than is the aerodynamic torque. However, for those cases where there is a bend upstream of the valve the torque is inputted directly. The program used for this is "FLOW-CL1".

#### SEISMIC ANALYSIS

The equations used for the seismic analysis are those given in Reference (c). The only difference between the seismic analyses performed in this report and those performed in Reference (c) is the analyses in this report use the torque resulting from a LOCA for input rather than operational torques.



DETAILED ANALYSISDetermination of LOCA Torques

Per Reference (d) when a Loss of Coolant Accident (LOCA) occurs the pressure inside containment will increase to 45 psig and 3.1 psig outside containment. The temperature inside of containment during an accident can range from 135 degrees F. to 340 degrees F., for outside containment the range is from 104 degrees F. to 275 degrees F.

To perform the LOCA analysis it is assumed for conservatism that the pressure drop across each piping system investigated is the full 45 psig. However, the actuators outside containment are subjected to the 3.1 psig.

Since the make up of the media is not known, three different conditions are analyzed using the first case to determine which condition results in the largest aerodynamic torques. This condition is then used in the analysis of the other piping systems. The three conditions investigated are as follows:

<u>Condition</u>	<u>Media</u>	<u>Temperature (Degrees F)</u>
1	Air	135
2	Air	340
3	Steam	292 (Saturated)

As can be seen in Appendix B, Condition 2 resulted in the largest torques.



The torques resulting from a LOCA based on Condition 2 are determined using the program "FLOW-GAS". The computer results can be seen in Appendix B on the pages as described below:

<u>Case</u>	<u>Page</u>	<u>Flow Direction</u>
1A	B-5	Preferred
1B	B-17	Nonpreferred
2A	B-24	Preferred
2B	B-29	Nonpreferred
3A	B-34	Nonpreferred
3B	B-38	Nonpreferred
4A	B-42	Preferred

As can be seen in Appendix A just upstream from valves AOV110 and AOV111 (Cases 2B & 4B) are bends. Therefore, the effects of these bends on the aerodynamic torques during a LOCA have to be determined.

Posi-Seal has performed an investigation to determine what effect a pipe bend will have. To date this investigation has not revealed anything Posi-Seal can use with confidence. Consequently, Posi-Seal has taken the following approach:

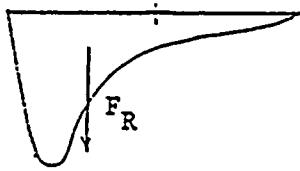
1. Assume the flow results in a resultant load acting at the midpoint between the edge of the disc and the stem centerline.
2. Determine the load based on the principles of impulse and momentum.
3. Calculate the resulting torque choosing the angle of attack which results in the worst case when added to the aerodynamic torque of the normal flow thru the valve.



The assumption that the flow resultant acts at the midpoint between the edge of the disc and the stem center line with a bend upstream is based on the following:

1. For flow through a straight pipe the largest aerodynamic torque will occur at 80 degrees open for flow in the preferred direction and 90 degrees for flow in the nonpreferred direction. This torque is predominately due to the lift and drag forces acting on the disc. Only a small amount of torque is due to the flow impacting on the disc since the moment arm is relatively small.
2. It is assumed that the resultant of the flow impacts the disc at the midpoint between the disc edge and the stem center line throughout the closure from 90 degrees open to fully closed. Although this may not be conservative at the smaller angles, it will result in very conservative results at 80 and 90 degrees where the maximum torques due to the lift and drag forces occur. See the diagram below.

Figure 7



Velocity profile with resultant acting at midpoint between disc edge and stem  $\S$



Valve at 80 degrees



Velocity profile acting on the disc at 80 degrees and the corresponding resultant.

Posi-Seal uses the full value of  $F_R$  throughout the valve closure.



The magnitude of the force impacting the disc is determined by using the principles of impulse and momentum as follows:

$$\Delta M V_1 + F \Delta t = \Delta M V_2$$

$$V_2 = 0$$

$$\Delta M V_1 = F \Delta t$$

where  $\Delta M$  = Change in mass - lbm

$V$  = Velocity - ft/sec

$F$  = Force - lbs

$\Delta t$  = Change in time

$$\Delta M = \frac{A \rho V \Delta t}{g}$$

where  $A$  = Area -  $ft^2$

$\rho$  = Density -  $lbm/ft^3$

$g$  = Gravitational Constant

$$W = A \rho V = Flow - lbs/sec$$

$$\frac{W V_1}{g} \Delta t = F \Delta t$$

$$F = \frac{W V_1}{g}$$

$$W = \frac{.0764 Q G}{3600}$$

where  $Q$  = Flow - SCFH

$$F = \frac{.0764 Q V}{32.2 (3600)} = \frac{Q V G}{1.517 \times 10^6}$$



DETERMINATION OF AERODYNAMIC TORQUES RESULTING FROM THE BENDSValve AOV110 (Case 2A)

The valve is orientated in the pipeline as shown below with the flow in the nonpreferred direction.

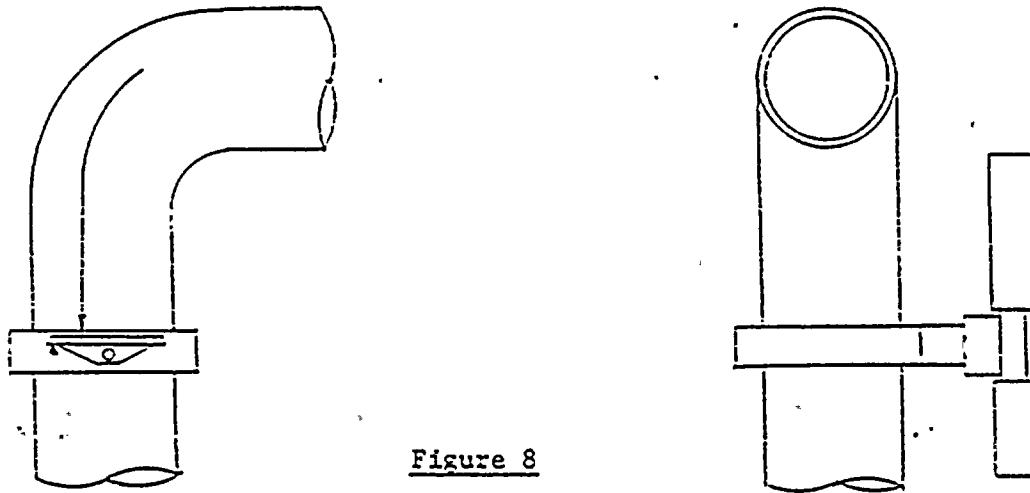


Figure 8

For this case, the resultant of the flow is assumed to be normal to the disc with the valve in the closed position. This is the most conservative assumption concerning the direction of the flow resultant since this assumes that when the valve is fully open that the flow will not assist in closing the valve.

Using this assumption the torques acting on valve AOV110 are calculated.

<u>Degree</u>	<u>Q</u> (Per Appendix B)	<u>V</u>	<u>E</u>
90	11,646,000	633.8	1941
80	4,470,000	642.2	1892
70	3,982,000	647.2	1699
60	3,068,000	619.7	1253
50	2,289,000	526.8	795
40	1,552,000	388.3	397
30	958,000	250.3	158
20	483,000	128.4	41
10	244,000	65.2	10



$$R = \frac{D}{4} \cos \theta = \frac{12.074}{4} \cos \theta$$

<u>Degree</u>	R	T <sub>R</sub>	T <sub>LOCA</sub>	T <sub>Total</sub>
(Per Appendix B)				
90	0	0	7287	7287
80	.56	-1060	1110	50
70	1.11	-1886	-780	-1106
60	1.62	-2030	337	-1693
50	2.08	-1654	1132	-522
40	2.48	-985	1348	363
30	2.81	-444	1414	970
20	3.05	-125	1440	1315
10	3.19	-32	1445	1413

A positive torque indicates that the valve will tend to remain open.

#### Valve AOV111 (Case 4B)

This valve is also presently mounted in the nonpreferred direction, orientated as shown below.

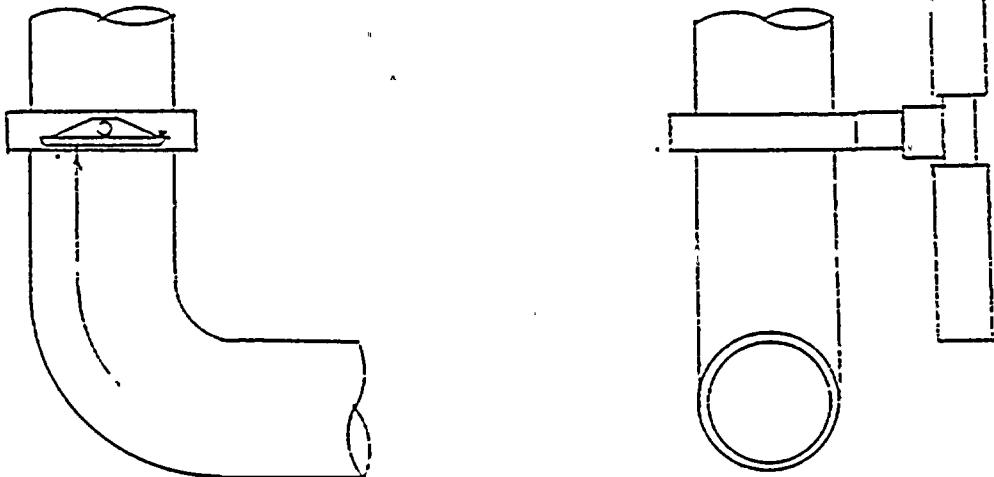


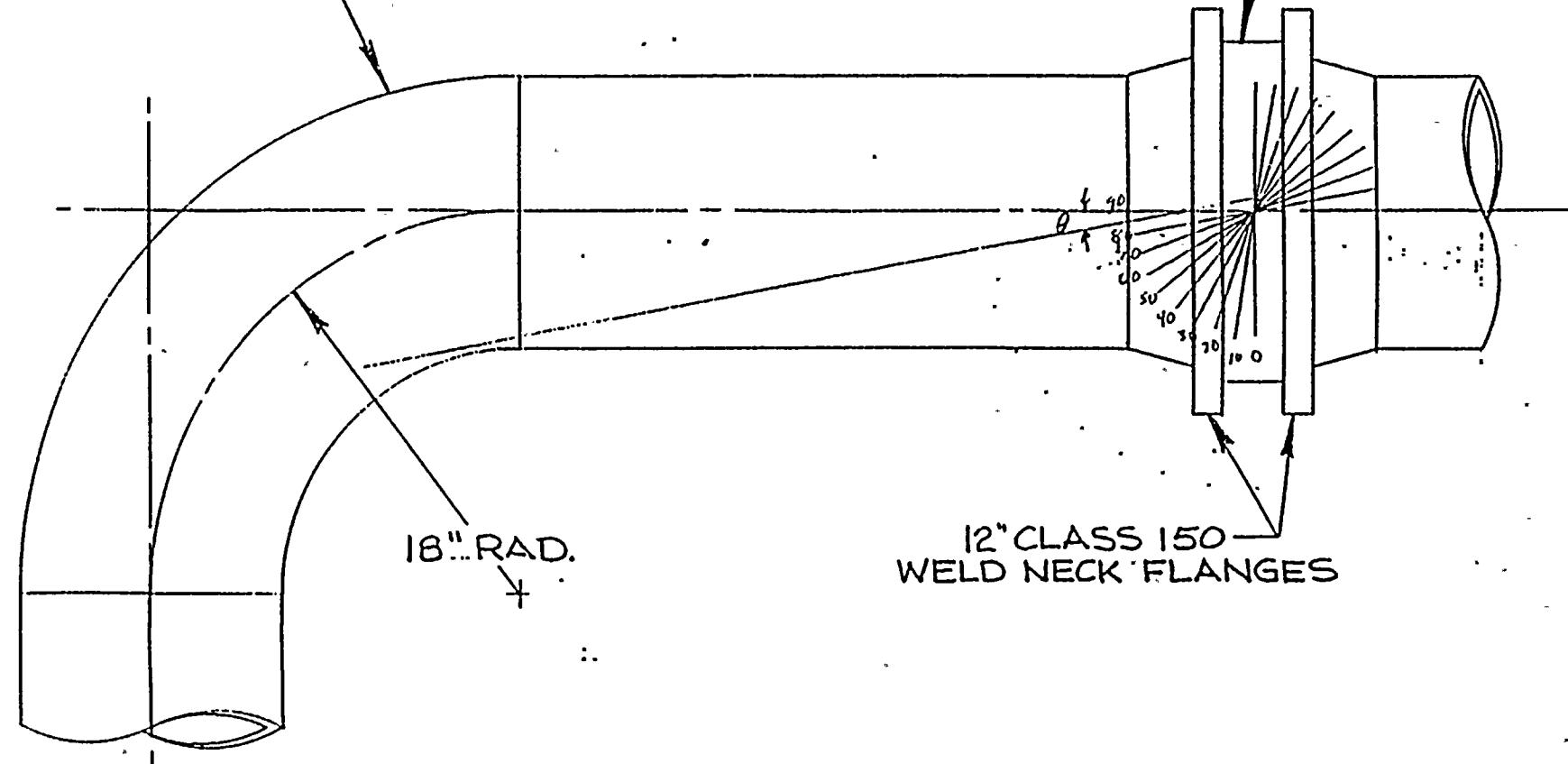
Figure 9

For this case the flow resultant is also assumed to act normal to the disc in the shut position except at 90 degrees where it is assumed to be in line with the tangent to the inside diameter of the elbow. See Figure 10 on Page 29.



90° LONG RADIUS  
WELDELL

12"/150 POSI-SEAL  
VALVE #2CPS-AOVIII



- 29 -

Figure 10

NINE MILE PT. NUCLEAR STA.-UNIT

VENTILATION REACTOR BLDG.  
AIR COOL & PURGE SECTIONS

SCALE  $\frac{1}{8}'' = 1'$



The calculated torques for valve AOV111 are as follows:

<u>Degree</u>	<u>Q</u> (Per Appendix B)	<u>V</u>	<u>E</u>
90	3,444,000	631.5	1434
80	3,444,000	720.1	1635
70	3,049,000	642.5	1291
60	2,376,000	632.0	990
50	1,785,000	548.3	645
40	1,212,000	409.2	327
30	749,000	265.4	131
20	377,000	136.6	34
10	191,000	69.4	9

$$R = \frac{D}{4} \cos \theta = \frac{11.703}{4} \cos \theta$$

except at 90 degrees  $R = \frac{11.703}{4} \sin (10 \text{ degrees})$

<u>Degree</u>	<u>R</u>	<u>T<sub>R</sub></u>	<u>T<sub>LOCA</sub></u> (Per Appendix B)	<u>T<sub>Total</sub></u>
90	.51	729	4446	5174
80	.51	834	964	1798
70	1.00	1291	- 180	1111
60	1.46	1445	495	1940
50	1.88	1213	996	2209
40	2.24	732	1141	1873
30	2.53	332	1187	855
20	2.75	93	1206	1113
10	2.88	25	1209	1234



### DETERMINATION OF CLOSING TIMES

Based on the aerodynamic torques determined in Appendix B and the preceding pages, the closing times are calculated using the computer programs "FLOW-CL" and "FLOW-CL1". The results of these calculations are shown in Appendix C.

As can be seen on Pages C-4, C-8 and C-16, valves AOV104, 110 and 111 will not close when subject to the torque resulting from a LOCA. Valve AOV105 takes greater than the 5 sec. closing requirement and valve AOV107, although it meets the 5 sec. requirement, takes twice as long to close as it normally does. See Pages C-10, C-12 and F-6.

All of the above valves are installed in the nonpreferred direction. Therefore, it is recommended that they be installed in the preferred direction.

The LOCA torque calculations for these valves are given on Pages B-52 thru B-73. For valves AOV110 and 111 which have bends upstream, the additional torques due to the bends are as follows:

#### AOV110 (Case 2B)

With this valve installed in the preferred direction it is recommended that the valve be orientated as shown below. With this orientation the direction of the flow resultant is assumed to be in line with the tangent to the inside diameter of the bend and the arc of the midpoint as the valve closes. See Figure 12 on Page 32.

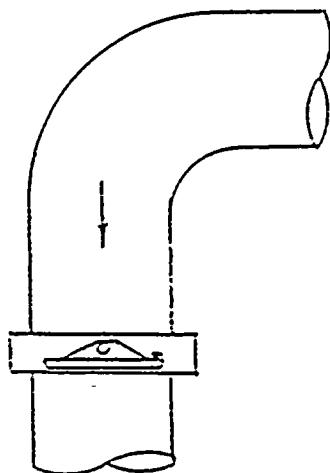
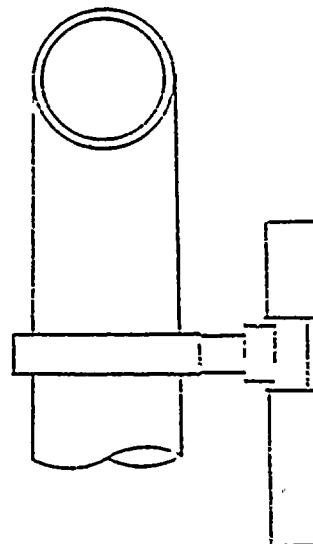


Figure 11





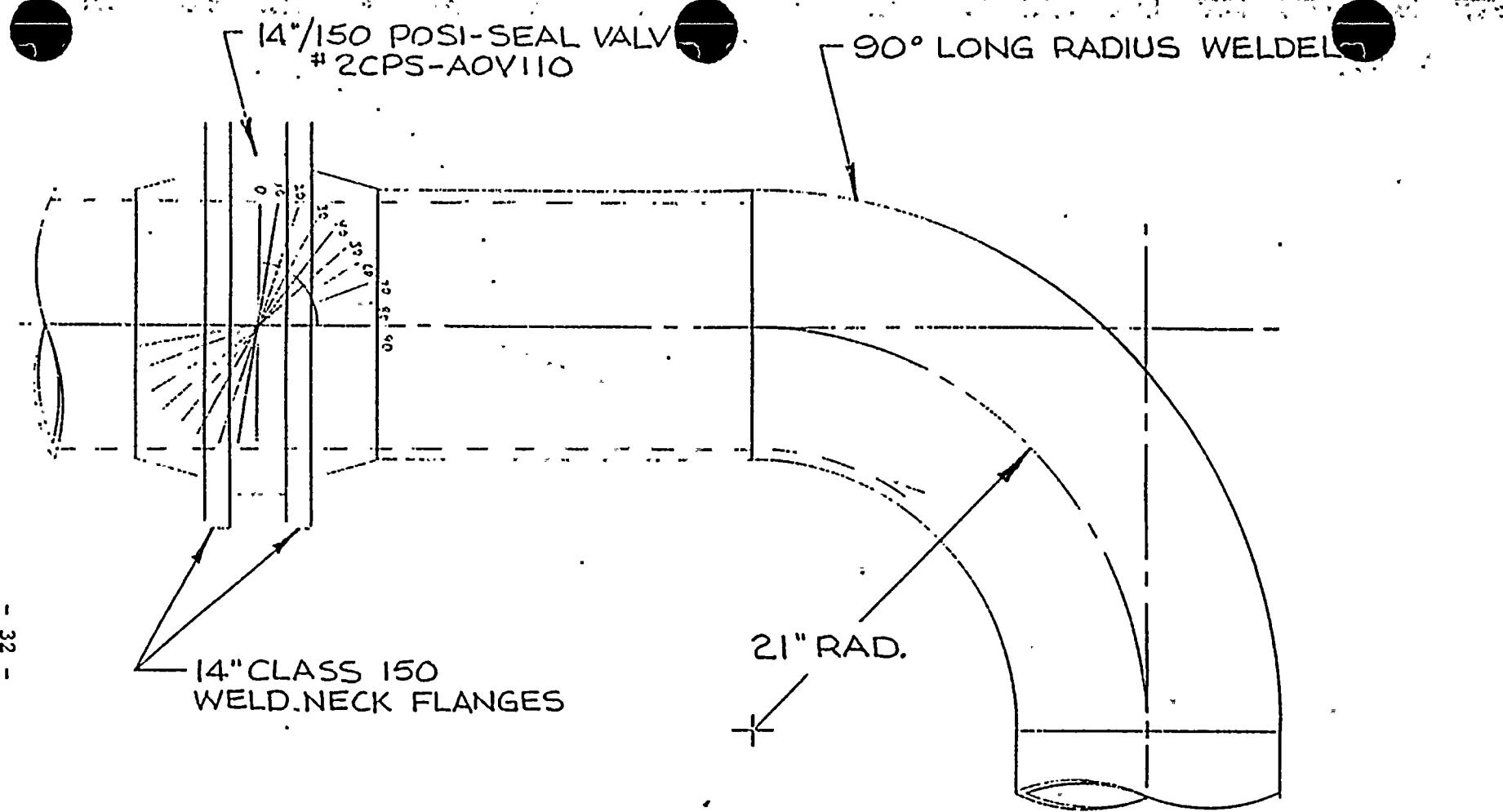


Figure 12

NINE MILE PT. NUCLEAR STA.-UNIT  
VENTILATION REACTOR BLDG.  
AIR COOL & PURGE SECTIONS

SCALE  $\frac{1}{8}$ " = 1'



This resultant direction is chosen since it results in the largest torques when added to the torques with the valve in the preferred direction. This represents the worst case, stress wise, in terms of the torque the valve assembly will be subject to. These torques are

$$R = D/4 \cos (20-6)$$

Degree	R	T <sub>R</sub>	T <sub>LOCA</sub>	T <sub>Total</sub>
(Per Appendix B)				
90	1.11	-2153	-5433	-7586
80	1.62	-3068	-6516	-9584
70	2.08	-3542	-3954	-7496
60	2.48	-3113	-730	-3113
50	2.81	-2233	741	-1492
40	3.05	-1210	1217	7
30	3.19	-504	1393	888
20	3.24	-133	1436	1303
10	3.19	-32	1445	1413

AOV111 (Case 4B)

It is recommended with this valve in the preferred direction it be orientated as shown below

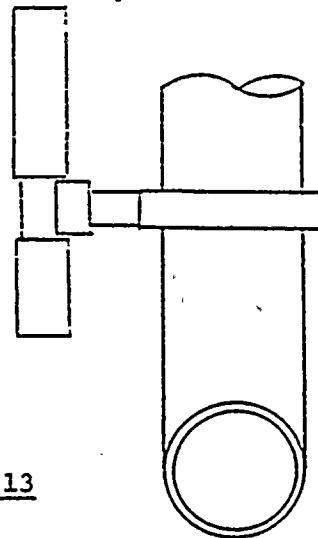
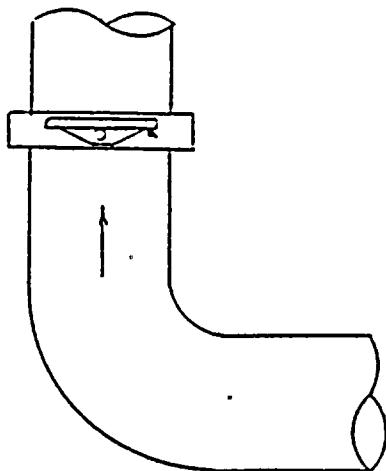


Figure 13



The direction of the flow resultant that results in the largest torque for this valve is the same as it is for valve AOV110. See Figure 14 on Page 35. Therefore, the torques are:

$$R = \frac{D}{4} \cos(20.6)$$

<u>Degree</u>	R	T <sub>R</sub>	T <sub>LOCA</sub>	T <sub>Total</sub>
(Per Appendix B)				
90	1.00	-1592	-2813	-4404
80	1.46	-2649	-4127	-6776
70	1.88	-2685	-2044	-4729
60	2.24	-2455	-156	-2611
50	2.53	-1812	751	-1061
40	2.74	-997	1058	61
30	2.88	-418	1174	756
20	2.93	-110	1203	1093
10	2.88	-29	1209	1180

The determination of the closing times for valves AOV104, 105, 107, 110 and 111 with flow in the preferred direction is given in Appendix D.

If these valves cannot be installed in the preferred direction, then it is recommended that the amount of valve opening be restricted to 70 degrees. Shown in Appendix E are the closing times for these valves with this restriction.



IE/150 Full-SEAL  
VALVE #2CPS-AOVIII

**SCHL JG RADIUS  
WELDELL**

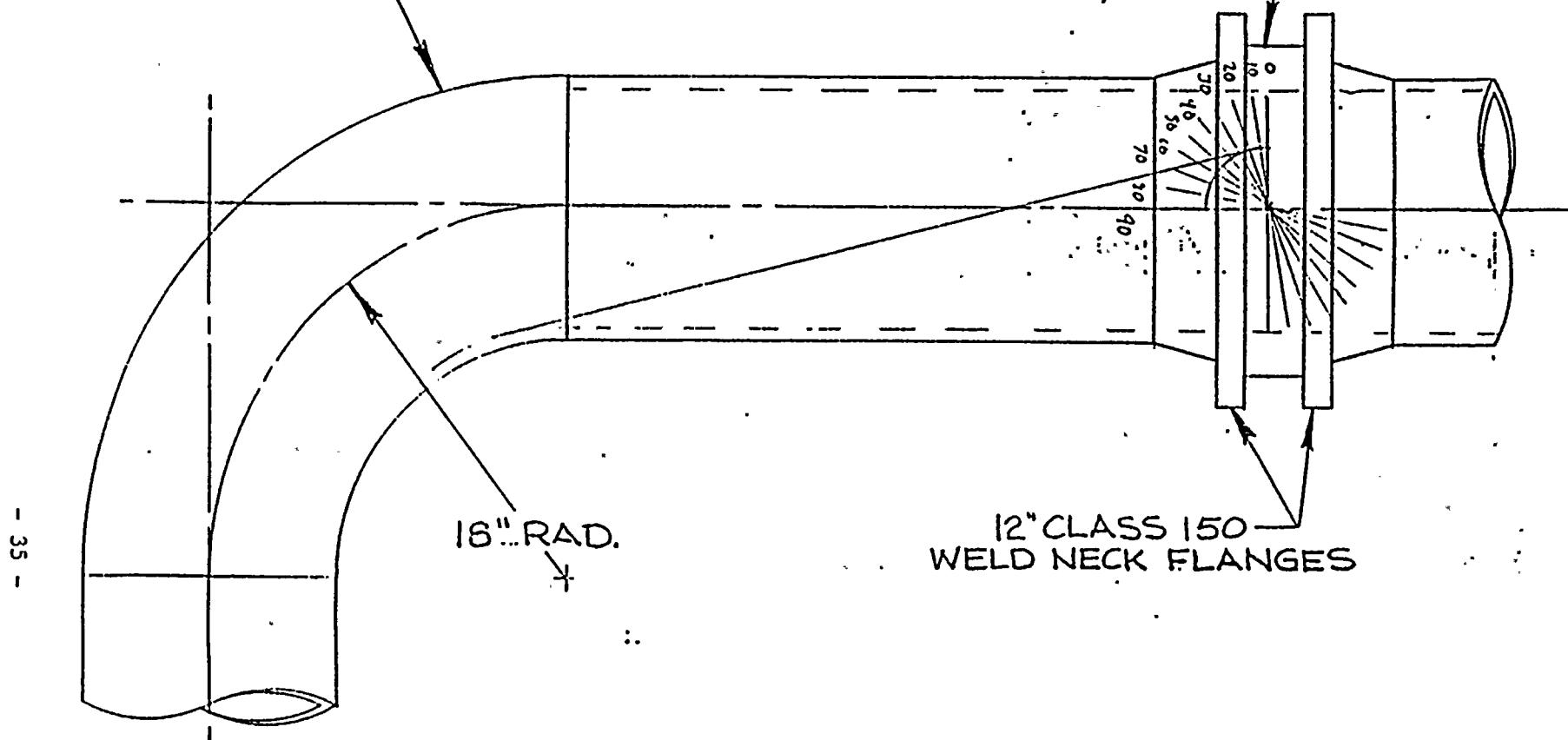
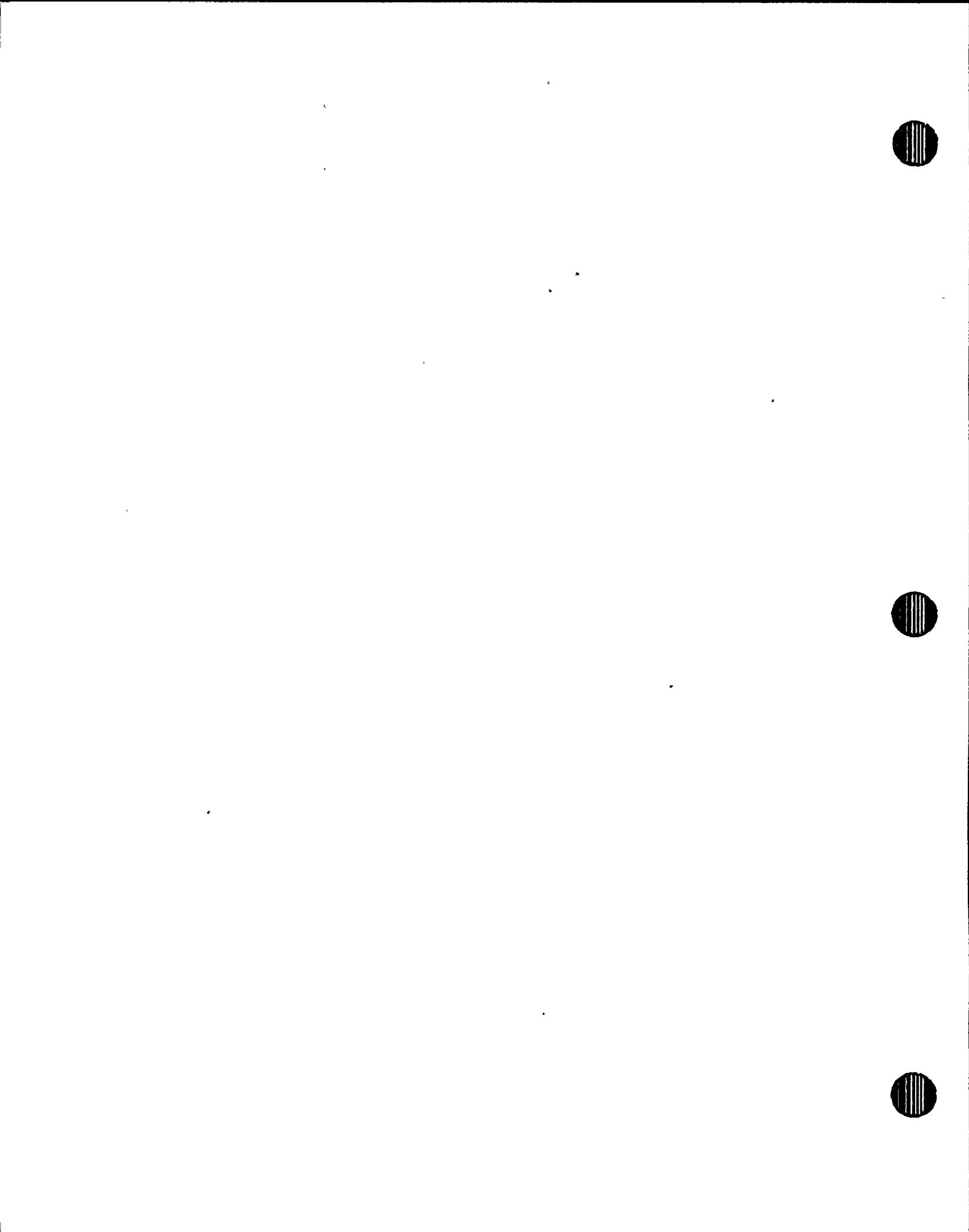


Figure 13

NINE MILE PT. NUCLEAR STA.-UNI

## VENTILATION REACTOR BLDG. AIR COOL & PURGE SECTIONS

SCALE  $\frac{1}{8}'' = 1'$



Seismic Analysis

For the seismic analysis of each individual valve, the conditions and orientations which resulted in the largest torques were used. They are as follows:

<u>Case</u>	<u>Valve</u>	<u>Valve Opening</u>	<u>Flow Direction</u>
1A	AOV106	80	Preferred
1B	AOV104	90	Nonpreferred
2A	AOV108	80	Preferred
2B	AOV110	80	Preferred
3A	AOV107	90	Nonpreferred
3B	AOV105	90	Nonpreferred
4A	AOV109	80	Preferred
4B	AOV111	80	Preferred

The seismic analyses are given in Appendix G. As can be seen on Page G-24 the disc pin stress for valve AOV111 exceeds the allowable; therefore, it is recommended the amount of valve opening for this valve be restricted to 70 degrees. The seismic analysis for this condition is given on Pages G-25 and G-26.



APPENDIX A

SCHEMATIC OF THE PIPING SYSTEM

NOTE: The orientation of the valves is  
based on the normal flow  
directions given on Posi-Seal  
assembly drawings, Enclosure (1).



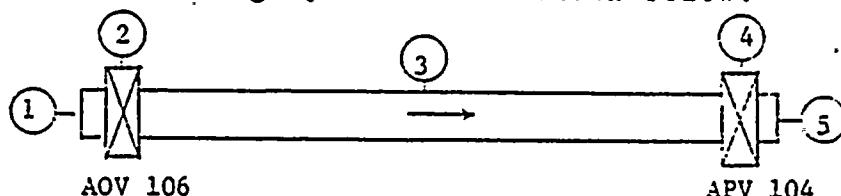
CASE 1

14" - 150 Class Valves 2CPS\*AOV 104 & 106

Worse Condition

Piping outboard of valve 2CPS\*AOV104 breaks off.

The resulting system is as shown below.



Per References  
(e) & (f)

<u>Station No.</u>	<u>Type of Resistance (No.)</u>	
1	Entrance (1)	$K = .5$ $D_{in} = 14"$
2	Valve (7) Flow in the Preferred Direction	$C_V = 6317$
3	Straight Pipe (4)	$L = 11'$
4	Valve (7) Flow in the Nonpreferred Direction	$C_V = 6317$
5	Exit (8)	$K = 1.0$ $D_{out} = 14"$

Case 1A - Valve AOV106 Cycles  
1B - Valve AOV104 Cycles



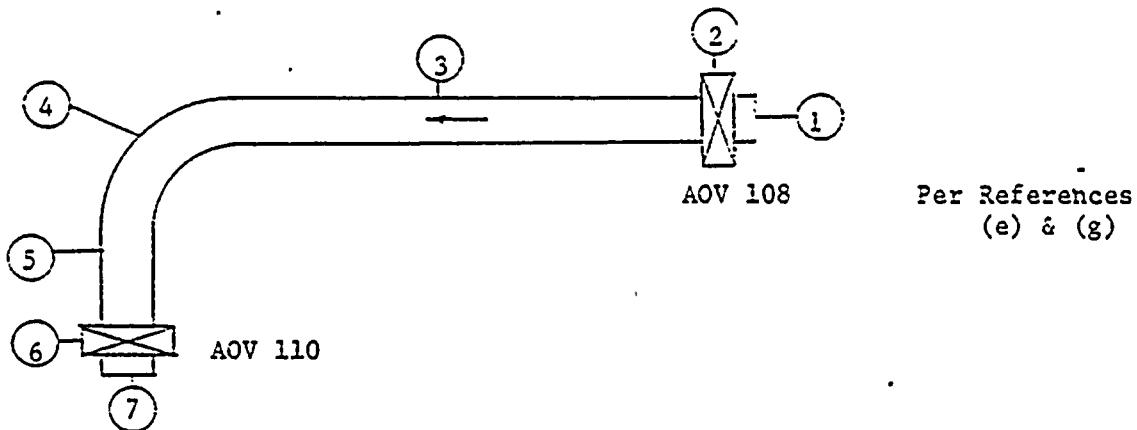
CASE 2

14" - 150 Class Valves 2CPS\*AOV 108 &amp; 110

Worse Condition

Piping outboard of valve 2CPS\*AOV110 breaks off.

The resulting system is as shown below.



<u>Station No.</u>	<u>Type of Resistance (No.)</u>	
1	Entrance (1)	$K = .5 \quad D_{in} = 14"$
2	Valve (7) Flow in the Preferred Direction	$C_V = 6317$
3	Straight Pipe (4)	$L = 9'$
4	Bend 90 Degrees (5)	$K = 12 \quad f_t = .16$
5	Straight Pipe (4)	$L = 3'$
6	Valve (7) Flow in the Nonpreferred Direction	$C_V = 6317$
7	Exit (8)	$K = 1 \quad D_{out} = 14"$

Case 2A - Valve AOV108 Cycles  
 2B - Valve AOV110 Cycles



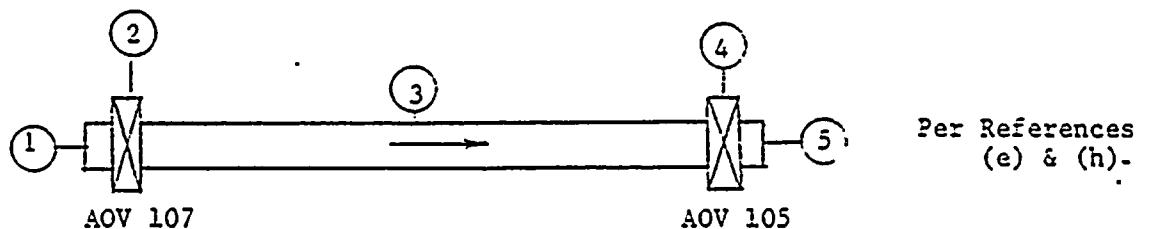
CASE 3

12" - 150 Class Valves 2CPS\*AOV 105 & 107

Worse Condition

Piping outboard of valve 2CPS\*AOV105 breaks off.

The resulting system is as shown below.



Station No.      Type of Resistance (No.)

1	Entrance (1)	$K = .5$ $D_{in} = 12"$
2	Valve (7) Flow in the Nonpreferred Direction	$C_V = 4942$
3	Straight Pipe (4)	$L = 11'$
4	Valve (7) Flow in the Nonpreferred Direction	$C_V = 4942$
5	Exit (8)	$K = 1$ $D_{out} = 12"$

Case 3A - Valve AOV107 Cycles  
3B - Valve AOV105 Cycles



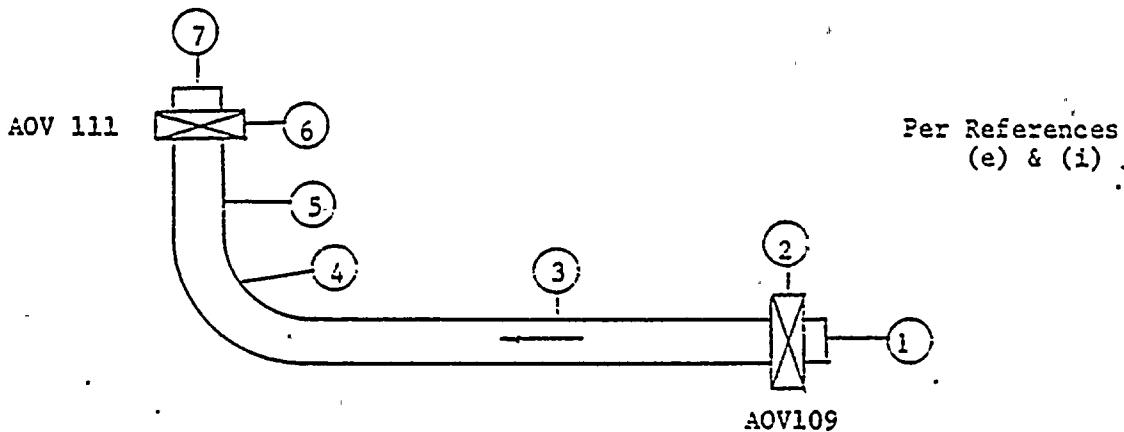
CASE 4

12" - 150 Class Valves 2CPS\*AOV 109 &amp; 111

Worse Condition

Piping outboard of valve 2CPS\*AOV111 breaks off.

The resulting system is as shown below.



<u>Station No.</u>	<u>Type of Resistance (No.)</u>	
1	Entrance (1)	$K = .5 \quad D_{in} = 12"$
2	Valve (7) Flow in the Preferred Direction	$C_V = 4942$
3	Straight Pipe (4)	$L = 9'$
4	Bend 90 Degrees (5)	$K = 12 \quad f_t = .16$
5	Straight Pipe (4)	$L = 4'$
6	Valve (7) Flow in the Nonpreferred Direction	$C_V = 4942$
7	Exit (8)	$K = 1 \quad D_{out} = 12"$

Case 4A - Valve AOV109 Cycles  
4B - Valve AOV111 Cycles



APPENDIX B

Determination of Flow Conditions



CASE 1A

CONDITION 1

NUCLEAR LCCA ANALYSIS

VALVE SIZE: 14"

VALVE CLASS: 150

ACTUATOR: Bell & Gossett N721C-SR30-M3H4V

UPSTREAM PRESSURE 59.7 PSIA

INITIAL DENSITY 2.71 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 135 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA Air

RATIO OF SP. HEAT 1.4

SPECIFIC GRAVITY 1.0

COMPRESSIBILITY 1

HYDRODYNAMIC FACTOR

θ 90 DEG 1182 IN. LBS  
PSI

STEM DIA. 1.375 IN.

GAGE DIA. 12.974 IN

PACKING TORQUE 832 IN. LBS.

SEAL TORQUE 1454 IN. LBS

DIRECTION Preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



**CONTROL SYSTEM ANALYSIS**

VALVE CLOSED		VALVE OPEN		FLOW RATE
UPSTREAM PRESSURE	INITIAL VELOCITY	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	27.1	135	14.7	59.7

MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	890 DEG 1182

STEM DIA.	GAGE DIA.	PACKING TORQUE	SEAL TORQUE
.00375	.02774	.032	.01574

STATION NO.	TYPE OF RESISTANCE	DIMMETER (D)	LENGTH (L)	RESISTANCE (R)	CORRECTED RESISTANCE (RC)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.350	0.36063
3	STRAIGHT PIPE	14.0	11.3	0.141	0.14142
4	VALVE	14.0	0.0	0.860	0.86063
5	EXIT	14.0	0.0	1.000	1.00000

**FLOW IN PREFERRED DIRECTION**

CONDITIONS WITH VALVE OPEN  
FLOW = 5,447,632 SCFH

STATION NO.	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	398.7
2	53.5	0.2506	130.8	430.7
3	49.0	0.2322	126.3	438.1
4	46.0	0.2252	125.3	478.3
5	39.1	0.2003	119.4	539.5
3	14.7	0.0973	70.4	1025.3

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE = 3.101 IN. LBS  
DELTAP = 45.00 PSI

1779



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	2,747,632	5.45	- 7,515	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	378.7
2	53.5	0.2505	130.8	430.7
3	48.0	0.2320	126.8	465.1
4	45.0	0.2231	120.3	479.5
5	39.1	0.2003	119.6	539.6
6	14.7	0.0995	90.4	1085.6

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	5,447,632	9.68	- 6,115	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	399.9
2	53.5	0.2505	130.8	430.7
3	43.8	0.2173	123.6	496.6
4	41.6	0.2095	121.7	514.4
5	32.9	0.1967	113.7	511.5
6	14.7	0.0995	90.4	1085.6

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
70	4,923,829	14.98	- 3,415	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	353.6
2	55.1	0.2561	131.9	373.6
3	40.2	0.2041	110.5	460.3
4	39.5	0.1983	119.1	481.5
5	31.6	0.1722	112.6	554.4
6	14.7	0.0995	90.4	1085.6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
60	3,708,674	29.57	- 613	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	271.6
2	57.2	0.2631	133.4	279.3
3	27.7	0.1588	103.4	467.7
4	26.6	0.1523	107.2	483.0
5	22.6	0.1357	102.3	542.1
6	14.7	0.0995	90.4	1085.6

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
50	2,711,930	37.75	- 752	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	198.6
2	58.5	0.2671	134.2	201.2
3	20.7	0.1274	99.8	422.3

5

2	15.3	0.1157	90.4	+0.0
2	14.7	0.0995	90.4	-0.0

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE °D	FLOW 1,812.99	DP ACROSS VALVE 42.07	Tclosing 1.215	
1	PRESSURE 59.7	DENSITY 0.2710	TEMPERATURE 135.0	VELOCITY 132.7
2	59.2	0.2706	134.7	133.2
3	17.2	0.1114	94.6	322.3
4	16.9	0.1104	94.2	325.3
5	16.7	0.1087	92.7	336.7
6	14.7	0.0995	90.4	361.1

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE 30	FLOW 1,109,994	DP ACROSS VALVE 43.97	Tclosing 1,391	
1	PRESSURE 59.7	DENSITY 0.2710	TEMPERATURE 135.0	81.2
2	59.6	0.2706	134.9	81.2
3	15.8	0.1040	92.0	211.7
4	15.5	0.1037	91.9	212.4
5	15.2	0.1021	91.3	215.6
6	14.7	0.0975	90.4	221.0

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE 20	FLOW 581.987	DP ACROSS VALVE 44.88	Tclosing 1,435	
1	PRESSURE 59.7	DENSITY 0.2710	TEMPERATURE 135.0	41.1
2	59.6	0.2709	134.9	41.1
3	15.0	0.1010	90.9	110.3
4	14.7	0.1007	90.9	110.4
5	14.8	0.1002	90.6	111.2
6	14.7	0.0995	90.4	112.0

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE 10	FLOW 284,134	DP ACROSS VALVE 44.91	Tclosing 1,444	
1	PRESSURE 59.7	DENSITY 0.2710	TEMPERATURE 135.0	20.8
2	59.5	0.2709	134.9	20.8
3	14.7	0.0999	90.5	56.4
4	14.7	0.0999	90.5	56.4
5	14.7	0.0997	90.5	56.5
6	14.7	0.0995	90.4	56.6

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 1A

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"  
VALVE CLASS: 150  
ACTUATOR: Bettis N721C - SR80 - M3HW

UPSTREAM PRESSURE 59.7 PSIA      INITIAL DENSITY .201 LB/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA Air  
.RATIO OF SP. HEAT 1.4      SPECIFIC GRAVITY 1  
COMPRESSIBILITY 1      HYDRODYNAMIC FACTOR  
@ 90 DEG 1182 IN.LB/S  
PSI

STEM DIA. 1.375 IN.      GAGE DIA. 12.474 IN.  
PACKING TORQUE 432 IN.LB.      SEAL TORQUE 1454 IN.LB  
DIRECTION Pr. flow

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



CONTROL SYSTEM ANALYSIS

VALVE SIZE=14		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE	INITIAL DENSITY-X10 <sup>+2</sup>	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	20.1	340	14.7	59.7

MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	1182
STEM DIA. 1.375	GAGE DIA. 12.974	PACKING TORQUE 832	SEAL TORQUE 1454	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.860	0.86066
3	STRAIGHT PIPE	14.0	11.0	0.141	0.14142
4	VALVE	14.0	0.0	0.350	0.35053
5	EXIT	14.0	0.0	1.000	1.00000

FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN

FLOW= 4,727,176 SCFM

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	57.7	0.2010	340.0	453.4
2	53.5	0.1860	329.6	501.6
3	48.0	0.1722	319.6	541.9
4	46.1	0.1572	313.7	558.4
5	39.2	0.1489	301.5	628.1
6	14.7	0.0738	227.8	1256.5

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT

VALVE TORQUE= 3,101 IN. LBS  
DELTA P=45.00 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW 7,727,745	DP ACROSS VALVE 1.45	Tclosing 4,322	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	435.4
2	53.5	0.1960	329.6	501.3
3	48.0	0.1722	319.6	541.9
4	46.1	0.1572	315.7	553.4
5	39.2	0.1489	301.5	528.1
6	14.7	0.0739	227.8	1266.6

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW 80 4,727,176	DP ACROSS VALVE 9.74	Tclosing - 6,170	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	465.4
2	53.5	0.1960	329.4	501.3
3	43.3	0.1611	311.2	579.0
4	41.7	0.1557	306.9	577.5
5	33.1	0.1321	297.3	708.0
6	14.7	0.0738	227.8	1266.6

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW 70 4,185,884	DP ACROSS VALVE 15.15	Tclosing - 3,450	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	412.1
2	55.2	0.1900	332.4	434.9
3	40.0	0.1511	303.3	548.9
4	38.4	0.1467	299.8	561.8
5	31.6	0.1277	283.6	645.4
6	14.7	0.0742	229.3	1201.7

ANGLE	FLOW 60 3,202,679	DP ACROSS VALVE 29.86	Tclosing - 622	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	315.3
2	57.3	0.1951	336.0	324.2
3	27.4	0.1153	275.2	547.5
4	26.4	0.1123	269.4	563.9
5	22.6	0.1006	257.8	629.7
6	14.7	0.0739	227.8	958.1

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW 50 2,839,792	DP ACROSS VALVE 37.74	Tclosing 792	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	230.4
2	56.5	0.1982	338.1	233.3
3	20.5	0.0939	250.8	492.8



2 13.7 0.0738 027.8 53.0  
3 13.7 0.0738 027.8 53.0

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
40	1,565,243	42.12	1,217
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2001	339.3
3	17.2	0.0826	238.2
4	16.9	0.0819	237.4
5	13.1	0.0791	234.2
6	14.7	0.0738	227.8
	VELOCITY		
1			154.1
2			154.3
3			374.3
4			373.1
5			371.3
6			419.4

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	957,243	44.00	1,392
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2007	339.3
3	15.6	0.0790	231.7
4	15.5	0.0768	231.4
5	15.2	0.0757	230.1
6	14.7	0.0738	227.3
	VELOCITY		
1			94.2
2			94.2
3			246.3
4			246.6
5			250.0
6			253.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	483,747	44.37	1,135
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2009	339.9
3	14.9	0.0749	229.1
4	14.7	0.0743	227.0
5	14.8	0.0743	228.4
6	14.7	0.0738	227.3
	VELOCITY		
1			47.9
2			47.6
3			127.7
4			127.7
5			128.7
6			129.6

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	244,569	44.91	1,444
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2009	339.7
3	14.7	0.0741	228.1
4	14.7	0.0741	228.1
5	14.7	0.0739	227.9
6	14.7	0.0738	227.8
	VELOCITY		
1			24.0
2			24.0
3			65.2
4			65.3
5			65.4
6			65.5

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 14

CONDITION 3

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"

VALVE CLASS: 150

ACTUATOR: Buttis N721C-SR80-M3HW

UPSTREAM PRESSURE 59.7 PSIA

INITIAL DENSITY .138 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 292 °F

FINAL PRESSURE .47 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA Sat. Steam

RATIO OF SP. HEAT 1.312

SPECIFIC GRAVITY .61

COMPRESSIBILITY 1

HYDRODYNAMIC FACTOR

@ 90 DEG 1182 IN.LBS  
PSI

STEM DIA. 1.375 IN.

GAGE DIA. 12.974 IN

PACKING TORQUE 932 IN.LBS.

SEAL TORQUE 1454 IN.LBS

DIRECTION Preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



VALVE SIZE=14		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE	INITIAL DENSITY-X10 <sup>+2</sup>	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	12.8	292	14.7	59.7
MEDIA	SATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
SAT. STEAM	1.312	.62	1	390-050
STEM DIA.	GAGE DIA.	PACKING TORQUE	SEAL TORQUE	1182
1.375	12.974	832	1454	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.860	0.86056
3	STRAIGHT PIPE	14.0	11.0	0.141	0.14142
4	VALVE	14.0	0.0	0.860	0.86056
5	EXIT	14.0	0.0	1.000	1.00000

FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN

FLOW= 3,375,.46 SCFH

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.1380	292.0	545.3
2	53.3	0.1266	284.2	592.9
3	48.3	0.1175	277.7	633.9
4	46.3	0.1141	275.1	555.3
5	40.3	0.1024	265.0	735.2
6	14.7	0.0474	209.2	1587.9

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT

VALVE TORQUE= 3,101 IN. LBS  
DELTA P=45.00 PSI

1702



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
0°	5,995,148	8.37	- 4,735
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.1380	292.0	488.3
2 53.3	0.1263	284.2	592.9
3 48.3	0.1175	277.7	638.9
4 43.5	0.1114	270.1	653.3
5 40.3	0.1024	266.0	735.2
6 14.7	0.0474	209.2	1597.9

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
60	5,895,146	8.77	- 5,739
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.1380	292.0	488.3
2 53.3	0.1263	284.2	592.9
3 44.5	0.1104	272.3	679.9
4 42.5	0.1065	269.3	702.2
5 35.2	0.0920	257.3	813.0
6 14.7	0.0474	209.2	1597.9

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	5,279,451	14.10	- 3,317
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.1380	292.0	488.3
2 54.9	0.1296	286.3	518.7
3 40.3	0.1034	236.3	650.2
4 39.3	0.1004	234.4	666.3
5 33.3	0.0884	254.1	757.0
6 14.7	0.0439	211.3	1354.1

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
60	4,057,308	29.47	- 630
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.1380	292.0	488.3
2 57.2	0.1336	289.1	586.7
3 57.2	0.0770	243.7	672.7
4 26.7	0.0747	241.1	693.2
5 23.3	0.0674	233.5	768.8
6 14.7	0.0474	209.2	1597.9

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	2,946,301	37.84	- 739
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.1380	292.0	488.3
2 58.6	0.1361	290.7	277.5
3 20.6	0.0615	226.9	615.7



15.2 20.707 20.7 200.0

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
-0	1,994.524	42.23	1,210
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.4	0.1379	291.9
3	17.2	0.0534	217.2
4	17.0	0.0530	216.6
5	13.2	0.0512	214.3
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	1,217.400	43.98	1,390
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.6	0.1378	291.8
3	15.5	0.0498	212.2
4	15.5	0.0494	212.0
5	15.2	0.0487	211.1
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
-0	615.18	44.67	1,435
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.6	0.1379	291.9
3	14.9	0.0481	210.2
4	14.7	0.0481	210.1
5	14.2	0.0477	209.7
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	311.010	44.91	1,444
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.6	0.1379	291.9
3	14.7	0.0476	209.5
4	14.7	0.0475	209.4
5	14.7	0.0475	209.3
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 1B

CONDITION 1

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"

VALVE CLASS: 150

ACTUATOR: B-44: N721C-SR80-M3HW

UPSTREAM PRESSURE 59.7 PSIA

INITIAL TEMPERATURE 135 °F

SHUT OFF PRESSURE 59.7 PSIA

RATIO OF SP. HEAT 1.4

COMPRESSIBILITY 1

INITIAL DENSITY .271 LBS/FT<sup>3</sup>

FINAL PRESSURE 14.1 PSIA

MEDIA Air

SPECIFIC GRAVITY 1.0

HYDRODYNAMIC FACTOR

@ 90 DEG 1182 IN.LBS  
PSI

STEM DIA. 1.375 IN.

GAGE DIA. 12.974 IN

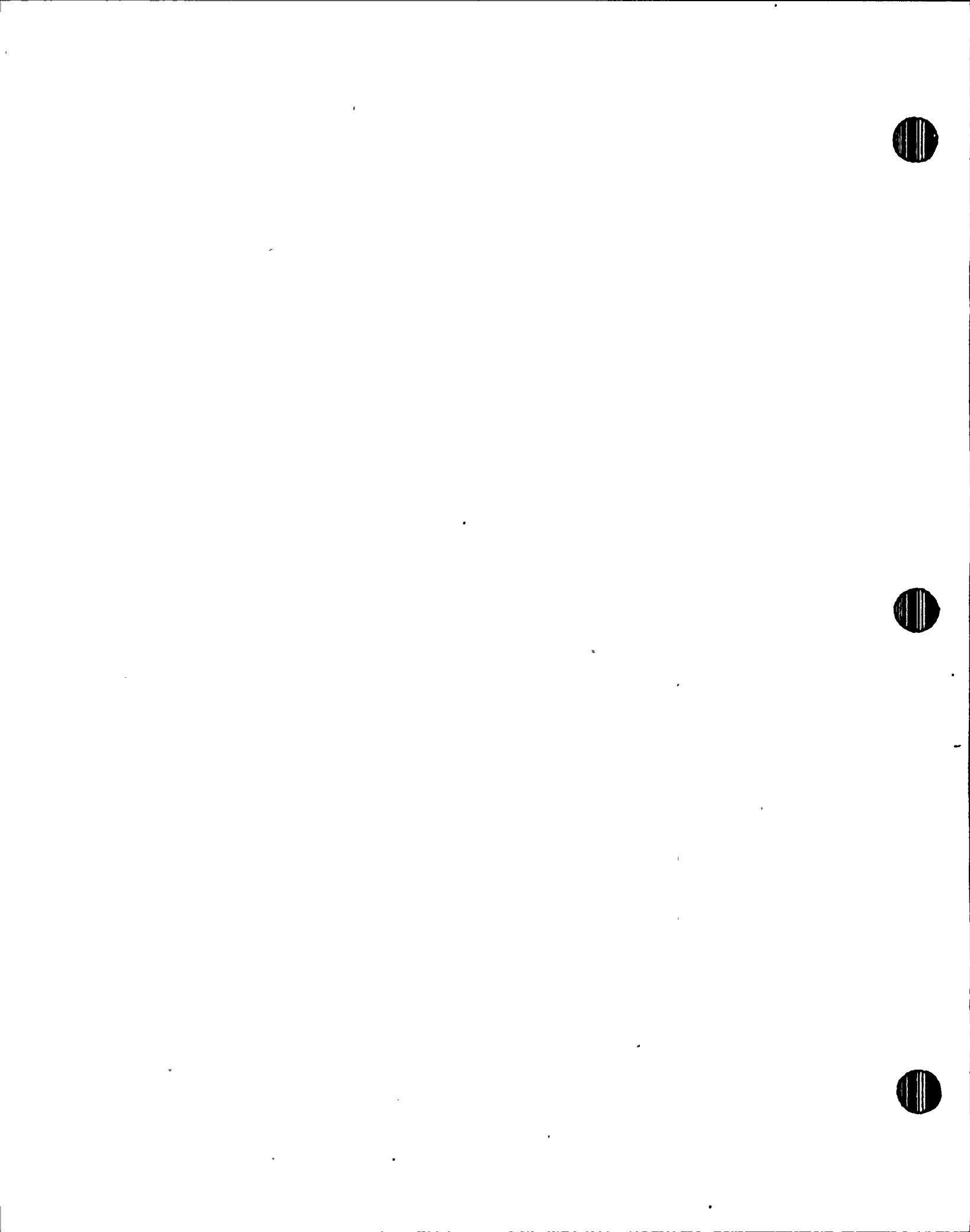
PACKING TORQUE 832 IN.LBS

SEAL TORQUE 14541 IN.LBS

DIRECTION Nonprefer.

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONTROL SYSTEM ANALYSIS

VALVE SIZE=14		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE	INITIAL DENSITY-X10+2	INITIAL TEMPERATURE,	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	27.2	135	14.7	59.7

MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	990 SEC
STEM DIA.	GAGE DIA.	PACKING TORQUE	SEAL TORQUE	
1.375	12.974	832	1454	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.860	0.86066
3	STRAIGHT PIPE	14.0	11.0	0.141	0.14142
4	VALVE	14.0	0.0	0.930	0.93053
5	EXIT	14.0	0.0	1.000	1.00000

## FLOW IN NONPREFERRED DIRECTION

## CONDITIONS WITH VALVE OPEN

FLOW= 5,447,532 SCFM

PRESSURE	DENSITY	TEMPERATURE	VELOCITY
59.7	0.2710	135.0	398.9
53.5	0.2506	130.8	430.7
48.0	0.2320	126.8	465.1
43.0	0.2252	123.3	473.3
39.1	0.2003	119.6	539.3
14.7	0.0995	90.4	1085.3

NOTE: THERE IS CHOKED FLOW AT STATION 5

## CONDITIONS WITH VALVE SHUT

VALVE TORQUE= 3,101 IN. LBS  
DELTA P=45.00 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
0	5,347,132	3.795	7,294
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2710	135.0	392.7
2 53.5	0.2506	130.3	430.7
3 48.0	0.2320	126.8	465.1
4 43.0	0.2162	123.3	479.5
5 39.1	0.2003	119.3	539.5
6 14.7	0.0995	90.4	1095.6

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
80	5,226,233	11.22	1,108
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2710	135.0	382.7
2 54.1	0.2525	131.2	409.9
3 49.2	0.2333	127.8	438.3
4 47.5	0.2304	126.5	448.7
5 36.3	0.1901	117.1	545.5
6 14.7	0.0995	90.4	1041.5

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	4,652,050	20.89	- 789
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2710	135.0	340.7
2 55.5	0.2575	132.2	357.3
3 52.0	0.2459	129.3	374.3
4 50.9	0.2419	129.0	380.2
5 30.0	0.1659	110.9	556.3
6 14.7	0.0995	90.4	927.1

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	3,337,092	35.10	333
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2710	135.0	261.0
2 57.4	0.2637	133.5	268.1
3 55.5	0.2574	132.2	274.6
4 55.0	0.2555	131.0	276.3
5 21.8	0.1323	101.3	534.7
6 14.7	0.0995	90.4	710.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	2,661,389	39.16	1,130
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2710	135.0	194.9

13.15



1	57.3	0.2710	135.0	170.3
2	57.3	0.2704	135.0	193.0
3	14.7	0.0995	90.4	530.3
4				

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
40	1,802,844	42.57	1,347

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	132.0
2	59.2	0.2696	134.7	132.5
3	58.3	0.2581	134.4	133.2
4	58.7	0.2679	134.3	133.2
5	16.1	0.1066	92.9	335.4
6	14.7	0.0995	90.4	339.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
30	2,113,243	44.13	1,414

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	81.5
2	59.6	0.2706	134.9	81.5
3	59.4	0.2701	134.9	81.6
4	59.4	0.2700	134.8	81.5
5	15.2	0.1021	91.3	216.2
6	14.7	0.0995	90.4	221.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
20	560,464	44.79	1,440

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	41.0
2	59.5	0.2707	134.7	41.0
3	59.4	0.2707	134.9	41.0
4	59.6	0.2707	134.9	41.0
5	14.3	0.1002	90.3	110.7
6	14.7	0.0995	90.4	111.6

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
10	283,334	44.94	1,445

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2710	135.0	20.7
2	59.6	0.2709	134.9	20.7
3	59.3	0.2709	134.7	20.7
4	59.6	0.2709	134.9	20.7
5	14.7	0.0997	90.5	56.3
6	14.7	0.0995	90.4	54.4

NOTE: THERE IS CHOKED FLOW AT STATION 4

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 1B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"  
VALVE CLASS: 150  
ACTUATOR: Bell & Gossett U721C-SR80-M3HW

UPSTREAM PRESSURE 59.7 PSIA      INITIAL DENSITY .201 LBS/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA Air  
RATIO OF SP. HEAT 1.4  
COMPRESSIBILITY 1      SPECIFIC GRAVITY 1.0  
HYDRODYNAMIC FACTOR  
90 DEG 1182 IN.LBS  
PSI

STEM DIA. 1.375 IN.  
PACKING TORQUE 332 IN.LBS.  
DIRECTION Non preferred  
GAGE DIA. 12.974 IN  
SEAL TORQUE 1454 IN.LBS

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONTROL SYSTEM ANALYSIS

VALVE SIZE=14		VALVE CLASS=150			FLOW-GAS
UPSTREAM PRESSURE 59.7	INITIAL DENSITY-Y1042 20.1	INITIAL TEMPERATURE 340	FINAL PRESSURE 14.7	SHUT-OFF PRESSURE 57.7	
MEDIA AIR	RATIO OF SP. HEAT 1.4	SPECIFIC GRAVITY 1	COMPRESSIBILITY 290-DEC	HYDRODYNAMIC FACTOR 1192	
STEM DIA. 1.375	CAE DIA. 12.974	PACKING TORQUE 832	SEAL TORQUE 1454		
STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.360	0.36066
3	STRAIGHT PIPE	14.0	11.0	0.141	0.14142
4	VALVE	14.0	0.0	0.250	0.25055
5	EXIT	14.0	0.0	1.000	1.00000

## FLOW IN NONPREFERRED DIRECTION

## CONDITIONS WITH VALVE OPEN

FLOW= 4,27,178 SCFM

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.1019	340.0	483.4
2	53.5	0.1860	329.6	501.6
3	48.0	0.1722	319.6	541.9
4	43.1	0.1372	315.7	553.4
5	39.2	0.1489	301.5	429.1
6	14.7	0.0733	227.8	1266.6

NOTE: THERE IS CHOKED FLOW AT STATION 5

## CONDITIONS WITH VALVE SHUT

VALVE TORQUE= 3,101 IN. LBS  
DELTA P=45.00 PSI



CONDITIONS AS VALVE CLOSES

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
90	1,727,173	3.92	7,337
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	53.5	0.1860	329.6
3	48.0	0.1722	319.6
4	43.1	0.1575	315.7
5	39.2	0.1489	301.5
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
80	4,530,955	11.10	1,107
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	54.1	0.1872	330.7
3	49.3	0.1754	321.9
4	47.6	0.1710	318.7
5	36.5	0.1415	305.7
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	4,030,437	20.69	- 795
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	55.6	0.1910	333.1
3	51.0	0.1822	325.7
4	50.9	0.1793	324.8
5	30.2	0.1235	279.8
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	3,065,312	33.24	531
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.5	0.1956	336.3
3	55.5	0.1910	333.1
4	55.0	0.1892	332.2
5	21.9	0.0982	255.3
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	2,302,002	39.28	1,131
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0



		0.1754	373.3	311.8
5	14.7	0.0738	227.3	315.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
40	1,551,983	42.64	1,349
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.3	0.2001	339.4
3	59.3	0.1990	338.5
4	58.8	0.1988	338.5
5	16.1	0.0790	234.1
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	930,301	44.13	1,724
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2007	339.8
3	59.4	0.2003	339.5
4	57.4	0.2002	339.5
5	15.2	0.0797	230.1
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	483,477	44.79	1,440
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.3	0.2007	337.7
3	59.6	0.2008	339.8
4	57.6	0.2008	339.8
5	14.3	0.0743	228.4
6	14.7	0.0738	227.9

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	244,414	44.94	1,445
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2009	339.9
3	57.6	0.2009	339.9
4	59.6	0.2009	339.9
5	14.7	0.0739	227.9
6	14.7	0.0738	227.9

NOTE: THERE IS CHOKED FLOW AT STATION 4

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 1B

CONDITION 3

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"

VALVE CLASS: 150

ACTUATOR: Bell & Gossett N721 C - SK80 - M34W

UPSTREAM PRESSURE 59.1 PSIA

INITIAL DENSITY 138 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 292 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.1 PSIA

MEDIA S.L. Steam

RATIO OF SP. HEAT 1.312

SPECIFIC GRAVITY .66

COMPRESSIBILITY 1

HYDRODYNAMIC FACTOR  
@ 90 DEG 1182 IN.LBS  
PSI

STEM DIA. 1.375 IN.

GAGE DIA. 12.974 IN.

PACKING TORQUE 832 IN.LBS

SEAL TORQUE 145Y IN.LBS

DIRECTION Non-preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



**CONTROL SYSTEM ANALYSIS**

VALVE SIZE=1/2" VALVE CLASS=150 SLOW-SAS-

UPSTREAM PRESSURE	INITIAL DENSITY	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	13.9	292	14.7	59.7
MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
SAT. STEAM	1.312	.62	1	390 DEG 1192
STEM DIA.	GAGE DIA.	PACKING TORQUE	SEAL TORQUE	
.375	.374	352	454	

STATION NO.	TYPE OF RESISTANCE	DIAMETER (D)	LENGTH (L)	RESISTANCE (K)	CORRECTED RESISTANCE (K)
1	ENTRANCE	14.0	0.0	0.500	0.5000
2	VALVE	14.0	0.0	0.860	0.8666
3	STRAIGHT PIPE	14.0	11.0	0.141	0.142
4	VALVE	14.0	0.0	0.360	0.3666
5	EXIT	14.0	0.0	1.000	1.0000

**FLOW IN NONPREFERRED DIRECTION**

CONDITIONS WITH VALVE OPEN  
FLOW = 5,895,146 SCFH

PRESSURE	DENSITY	TEMPERATURE	VELOCITY
59.7	0.1380	292.0	545.3
53.3	0.1266	284.2	592.9
48.3	0.1175	277.7	639.9
46.5	0.1141	275.1	655.3
40.3	0.1024	266.0	735.2
14.7	0.0474	207.2	1587.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE = 3,101 IN. LBS  
DELTAP = 43.00 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
90	5,895,146	37.14	373.9
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	55.3	0.1266	284.2
3	48.3	0.1175	277.7
4	46.5	0.1141	275.1
5	40.3	0.1024	266.0
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
90	5,895,146	13.62	1,159
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	55.3	0.1266	284.2
3	48.3	0.1175	277.7
4	46.5	0.1141	275.1
5	32.4	0.0866	253.3
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	5,118,788	18.69	743
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	55.4	0.1305	286.9
3	51.1	0.1245	282.7
4	51.1	0.1225	281.4
5	32.4	0.0866	252.5
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
60	3,701,590	32.66	320
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	57.5	0.1341	289.4
3	55.7	0.1309	287.2
4	55.7	0.1309	286.3
5	22.5	0.0657	231.7
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	2,910,489	39.14	1,125
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0



1	57.5	0.1342	239.1	575.7
2	59.4	0.1352	219.7	560.5
3	14.7	0.0474	209.2	564.0

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
40	1,974,411	42.70	1,347
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.4	0.1375	291.7
3	59.0	0.1358	291.1
4	58.9	0.1356	291.1
5	16.2	0.0511	214.2
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	1,217,379	44.15	1,413
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1390	292.0
2	59.6	0.1378	291.8
3	59.4	0.1375	291.7
4	59.4	0.1375	291.7
5	15.2	0.0487	211.1
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	613,001	44.78	1,440
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.5	0.1379	291.9
3	59.4	0.1378	291.9
4	59.4	0.1378	291.9
5	14.8	0.0472	209.7
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	309,891	44.94	1,445
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.1380	292.0
2	59.6	0.1379	291.9
3	59.6	0.1379	291.9
4	59.6	0.1379	291.9
5	14.7	0.0475	209.3
6	14.7	0.0474	209.2

NOTE: THERE IS CHOKED FLOW AT STATION 4

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 2A

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"  
VALVE CLASS: 150  
ACTUATOR: Bell: 11721C - SR80 - M3HW

UPSTREAM PRESSURE 59.7 PSIA      INITIAL DENSITY .201 LBS/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA Air  
RATIO OF SP. HEAT 1.4      SPECIFIC GRAVITY 1  
COMPRESSIBILITY ,      HYDRODYNAMIC FACTOR  
θ 90 DEG 1182 IN.LBS  
PSI

STEM DIA. 1.375 IN.      GAGE DIA. 12.974 IN  
PACKING TORQUE 932 IN.LBS.      SEAL TORQUE 1454 IN.LBS  
DIRECTION Proximal

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONTROL SYSTEM ANALYSIS

VALVE SIZE=14		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE 59.7	INITIAL DENSITY-X10^2 20.2	INITIAL TEMPERATURE 340	FINAL PRESSURE 2477	SHUT-OFF PRESSURE 34.7
MEDIA AIR	RATIO OF SF. VENT 1.4	SPECIFIC GRAVITY 1	COMPRESSIBILITY 890.020	HYDRODYNAMIC FACTOR 1182
STEM DIA. 1.375	GAGE DIA. 12.974	PACKING TORQUE 832	SEAL TORQUE 1454	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.860	0.86066
3	STRAIGHT PIPE	14.0	9.0	0.115	0.11571
4	PIPE BEND	14.0	0.0	0.150	0.15000
5	STRAIGHT PIPE	14.0	3.0	0.038	0.03857
6	VALVE	14.0	0.0	0.360	0.36066
7	EXIT	14.0	0.0	1.000	1.00000

## FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN  
FLOW= 4,645.997 SCFH

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.3010	340.0	457.5
2	53.7	0.1833	330.0	471.7
3	48.5	0.1734	320.5	528.9
4	47.2	0.1699	317.9	538.2
5	45.1	0.1543	313.3	554.3
6	44.7	0.1636	313.1	556.2
7	37.8	0.1450	298.4	633.8
8	34.7	0.0733	227.3	2244.9

NOTE: THERE IS CHOKED FLOW AT STATION 7

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE= 3,101 IN. LBS  
DELTA P=5.00 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	4,645,997	9.22	- 4,393	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	457.5
2	53.7	0.1966	330.0	491.7
3	48.5	0.1734	320.5	528.9
4	47.2	0.1579	317.9	538.1
5	45.1	0.1465	313.8	554.5
6	44.7	0.1353	313.1	556.2
7	37.3	0.1430	298.4	533.8
8	14.7	0.0738	227.9	1244.9

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	4,645,997	9.13	- 5,848	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	457.5
2	53.7	0.1866	330.0	491.7
3	44.3	0.1493	317.7	531.3
4	43.1	0.1593	309.8	573.9
5	40.8	0.1534	305.1	594.4
6	40.3	0.1524	304.4	576.4
7	31.8	0.1281	284.0	717.3
8	14.7	0.0738	227.9	1244.9

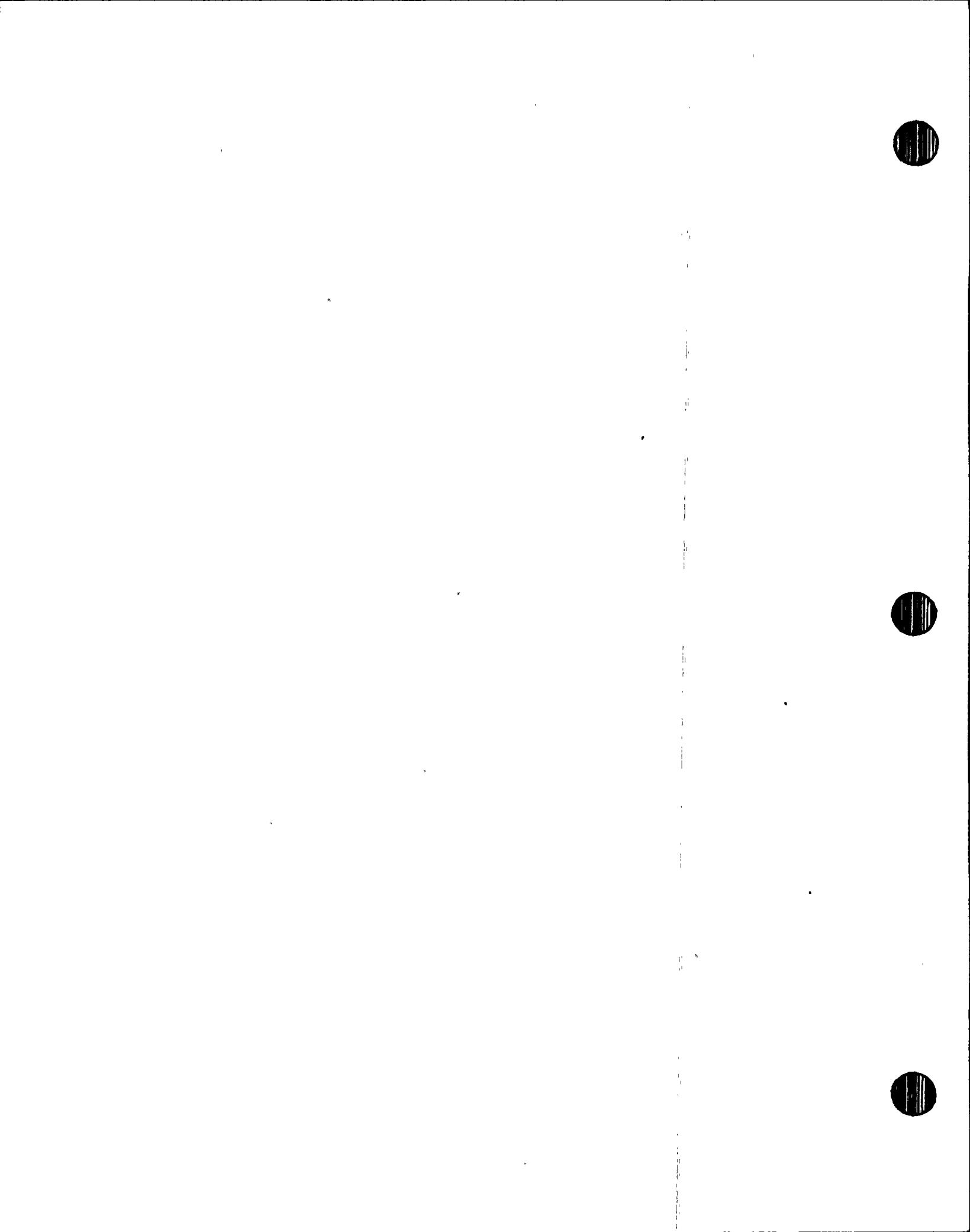
NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
70	4,142,038	14.35	- 3,307	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	407.3
2	53.2	0.1901	332.3	430.3
3	40.9	0.1534	305.1	533.4
4	39.6	0.1501	302.5	544.1
5	27.3	0.1492	298.5	560.9
6	37.5	0.1444	297.8	562.3
7	30.7	0.1251	281.1	655.0
8	14.7	0.0738	227.9	1209.3

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	3,294,783	13.71	- 537	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	315.5
2	57.2	0.1951	336.0	324.4
3	29.5	0.1187	290.3	534.0
4	27.3	0.1133	278.4	543.7
5	26.7	0.1132	270.2	560.0
6	26.5	0.1129	269.8	562.2
7	22.3	0.1006	257.3	557.7
8	14.7	0.0738	227.8	858.7

NOTE: THERE IS CHOKED FLOW AT STATION 7



ANGLE	FLOW	OP ACROSS VALVE	Tclosing
50	2,339,508	37.40	756
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0
2	58.5	0.1982	333.1
3	21.1	0.0937	222.7
4	20.7	0.0944	251.3
5	20.1	0.0925	249.3
6	20.0	0.0922	247.0
7	19.3	0.0865	242.7
8	14.7	0.0738	227.9

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	OP ACROSS VALVE	Tclosing
40	1,568,965	41.92	1,215
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0
2	59.3	0.2001	339.3
3	17.4	0.0833	239.0
4	17.2	0.0828	238.4
5	17.0	0.0820	237.5
6	16.9	0.0818	237.3
7	16.2	0.0791	234.2
8	14.7	0.0739	227.9

NOTE: THERE IS CHOKED FLOW AT STATION 3

ANGLE	FLOW	OP ACROSS VALVE	Tclosing
30	959,472	43.99	1,390
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	39.7	0.2010	340.0
2	59.6	0.2007	339.8
3	15.7	0.0774	232.1
4	15.3	0.0772	231.7
5	15.5	0.0769	231.6
6	15.5	0.0759	231.5
7	13.2	0.0737	230.1
8	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	OP ACROSS VALVE	Tclosing
20	485,258	44.65	1,435
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0
2	59.6	0.2009	339.9
3	15.0	0.0750	229.3
4	15.0	0.0749	229.1
5	14.9	0.0748	229.0
6	14.9	0.0740	229.0
7	14.9	0.0743	228.4
8	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 2



ANGLE 10	FLOW 245.337	OF VALVE	10.05113	
		22.91	1.444	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	24.1
2	59.5	0.2000	339.9	24.1
3	14.7	0.0731	229.1	65.4
4	14.7	0.0741	229.1	65.4
5	14.7	0.0741	229.1	65.4
6	14.7	0.0741	229.1	65.5
7	14.7	0.0739	227.9	65.6
8	14.7	0.0738	227.8	65.7

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 2B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"

VALVE CLAS: 150

ACTUATOR: Bell & *N721C-SR50-M3HW*

UPSTREAM PRESSURE 59.7 PSIA

INITIAL DENSITY .201 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 340 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA LI

RATIO OF SP. HEAT .64

SPECIFIC GRAVITY 1

COMPRESSIBILITY .1

HYDRODYNAMIC FACTOR

@ 90 DEG .1182 IN.LBS  
PSI

STEM DIA. .1375 IN.

GAGE DIA. .12.974 IN

PACKING TORQUE 832 IN.LBS.

SEAL TORQUE 1454 IN.LBS

DIRECTION No preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONTROL SYSTEM ANALYSIS

VALVE SIZE=14		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE	INITIAL DENSITY-X10+2	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	20.1	340	14.7	59.7
MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	290 SEC
STEM DIA.	GAUGE DIA.	PACKING TORQUE	SEAL TORQUE	
1.375	12.974	832	1454	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.860	0.36066
3	STRAIGHT PIPE	14.0	9.0	0.115	0.11571
4	PIPE 3EMO	14.0	0.0	0.286	0.14000
5	STRAIGHT PIPE	14.0	3.0	0.038	0.03857
6	VALVE	14.0	0.0	0.860	0.36066
7	EXIT	14.0	0.0	1.000	1.00000

## FLOW IN NONPREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN  
FLOW= 4,645,997 SCFH

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	457.5
2	53.7	0.1233	330.0	491.7
3	48.5	0.1734	320.5	528.9
4	47.2	0.1699	317.9	538.2
5	45.1	0.1843	313.8	554.5
6	44.7	0.1636	313.1	556.2
7	37.8	0.1450	298.4	633.8
8	14.7	0.0733	227.3	1244.7

NOTE: THERE IS CHOKED FLOW AT STATION 7

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE= 3,101 IN. LBS  
DELTA P=45.00 PSI



**CONDITIONS AS VALVE CLOSES.**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	4,469,962	0.05	7,287	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	457.5
2	53.7	0.1966	330.0	491.7
3	48.5	0.1734	320.5	528.9
4	47.2	0.1590	317.7	538.2
5	45.1	0.1645	313.8	554.5
6	44.7	0.1636	313.1	556.2
7	37.8	0.1460	298.4	338.3
8	14.7	0.0738	227.8	1244.9

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	4,469,962	11.29	1,110	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	440.1
2	54.3	0.1980	331.0	469.3
3	49.7	0.1763	322.6	500.4
4	48.5	0.1733	320.4	507.6
5	46.6	0.1685	316.8	521.2
6	46.4	0.1699	315.5	521.2
7	35.1	0.1377	292.1	642.2
8	14.7	0.0739	227.8	1197.7

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	3,982,860	20.51	780	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	392.1
2	55.3	0.1911	333.2	411.3
3	52.2	0.1827	327.2	430.7
4	51.4	0.1807	325.8	434.2
5	50.1	0.1777	323.3	440.3
6	50.1	0.1774	323.4	440.3
7	29.6	0.1217	278.2	647.2
8	14.7	0.0739	227.8	1037.2

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	3,060,311	32.93	537	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	302.1
2	57.6	0.1960	336.5	309.0
3	55.7	0.1914	333.4	316.3
4	55.1	0.1905	332.3	317.1
5	54.8	0.1892	331.8	318.9
6	54.7	0.1890	331.7	318.9
7	21.8	0.0979	255.0	319.7
8	14.7	0.0738	227.8	822.1

NOTE: THERE IS CHOKED FLOW AT STATION 4



ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
50	2,298.648	39.15	1,132	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	225.3
2	59.6	0.1985	338.3	227.4
3	57.3	0.1951	336.3	230.4
4	57.5	0.1958	336.4	230.4
5	57.3	0.1953	336.1	230.4
6	57.3	0.1952	336.0	230.4
7	18.1	0.0859	242.0	526.8
8	14.7	0.0738	227.9	613.2

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
40	1,651.568	42.55	1,348	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	152.7
2	59.3	0.2001	339.4	153.1
3	58.8	0.1990	338.6	153.9
4	58.8	0.1989	338.5	153.9
5	58.7	0.1987	338.4	153.9
6	58.7	0.1986	338.4	153.9
7	16.1	0.0790	234.1	388.3
8	14.7	0.0739	227.9	456.7

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
30	793.471	44.13	1,414	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	94.3
2	59.6	0.2007	339.8	94.3
3	59.4	0.2003	339.5	94.5
4	59.4	0.2003	339.5	94.3
5	59.3	0.2002	339.4	94.5
6	59.3	0.2002	339.4	94.5
7	18.5	0.0752	230.1	230.3
8	14.7	0.0739	227.8	266.8

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
20	482.546	44.78	1,440	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	47.5
2	59.6	0.2009	339.9	47.5
3	59.5	0.2008	339.8	47.5
4	59.6	0.2008	339.8	47.5
5	59.6	0.2008	339.8	47.5
6	59.5	0.2008	339.8	47.5
7	14.8	0.0743	228.3	128.4
8	14.7	0.0738	227.9	129.3

NOTE: THERE IS CHOKED FLOW AT STATION 6



ANGLE 10	FLOW 243,940	DP ACROSS VALVE 44.34	CLOSING 1,445	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	24.0
2	59.3	0.2007	339.7	24.0
3	59.6	0.2009	339.9	24.0
4	59.5	0.2009	339.9	24.0
5	59.3	0.2009	339.7	24.0
6	59.6	0.2009	339.9	24.0
7	14.7	0.0739	227.9	65.2
8	24.7	0.0733	227.3	65.3

NOTE: THERE IS CHOKED FLOW AT STATION 6

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 3A

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: Bell: N721C-SR80-M3HW

UPSTREAM PRESSURE 59.7 PSIA      INITIAL DENSITY .201 LBS/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA Air  
RATIO OF SP. HEAT 1.4  
COMPRESSIBILITY 1  
SPECIFIC GRAVITY 1  
HYDRODYNAMIC FACTOR  
@ 90 DEG 761 IN.LBS  
PSI

STEM DIA. .125 IN.  
PACKING TORQUE 756 IN.LBS.  
DIRECTION Upward  
GAGE DIA. .11.703 IN.  
SEAL TORQUE 1183 IN.LBS

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



CONTROL SYSTEM ANALYSIS

VALVE SIZE=12		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE	INITIAL DENSITY-X10+2	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	20.1	340	14.7	59.7
MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	990-000
STEM DIA.	GAGE DIA.	PACKING TORQUE	SEAL TORQUE	
1.25	11.703	756	1183	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	12.0	0.0	0.500	0.50000
2	VALVE	12.0	0.0	0.759	0.75903
3	STRAIGHT PIPE	12.0	11.0	0.165	0.16500
4	VALVE	12.0	0.0	0.759	0.75903
5	EXIT	12.0	0.0	1.000	1.00000

FLOW IN NON-REFINED DIRECTION

CONDITIONS WITH VALVE OPEN

FLOW = 3,617,147 SCFM

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	471.4
2	53.3	0.1855	329.2	509.4
3	48.5	0.1732	320.4	545.4
4	46.1	0.1675	315.2	583.2
5	40.2	0.1516	303.6	624.9
6	14.7	0.0738	227.8	1292.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT

VALVE TORQUE = 2,542 IN. LBS

DELTA P=45.00 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	3,517,149	4.39	3,449
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	53.3	0.1955	329.2
3	48.5	0.1732	320.4
4	46.1	0.1573	315.9
5	40.2	0.1516	303.6
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
80	3,517,149	8.39	908
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	53.3	0.1955	329.2
3	44.9	0.1641	313.5
4	42.3	0.1573	308.2
5	35.4	0.1384	277.7
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	3,173,985	13.52	- 103
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	54.8	0.1890	331.7
3	41.3	0.1544	305.9
4	39.2	0.1490	301.6
5	33.3	0.1326	287.8
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	2,174,313	27.74	303
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.0	0.1945	335.5
3	29.0	0.1202	276.8
4	27.7	0.1133	273.2
5	24.0	0.1050	262.2
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	1,823,803	37.17	991
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0



1	21.2	0.0051	453.1	510.7
2	20.5	0.0039	250.9	522.7
3	19.3	0.0033	247.1	535.0
4	14.7	0.0738	227.3	665.1

NOTE: THERE IS CHOKED FLOW AT STATION 2.

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
40	1,236,814	41.90	1,137
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.2	0.2000	339.3
3	17.4	0.0933	237.4
4	17.2	0.0826	238.3
5	16.4	0.0799	235.1
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	748,810	43.39	1,184
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2007	339.3
3	15.7	0.0774	232.1
4	15.8	0.0770	231.7
5	15.3	0.0760	230.4
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	378,407	44.65	1,205
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2007	339.3
3	15.0	0.0750	229.2
4	14.9	0.0749	229.1
5	14.3	0.0744	223.4
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	191,313	44.91	1,209
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2009	339.9
3	14.7	0.0741	228.1
4	14.7	0.0741	228.1
5	14.7	0.0740	227.9
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 3 B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 12  
VALVE CLASS: 150  
ACTUATOR: Bell & Gossett 11721C-3A80-M3HW

UPSTREAM PRESSURE 59.7 PSIA      INITIAL DENSITY .201 LBS/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA Air  
RATIO OF SP. HEAT 1.4  
COMPRESSIBILITY 1  
SPECIFIC GRAVITY 1  
HYDRODYNAMIC FACTOR  
@ 90 DEG 761 IN.LBS  
PSI

STEM DIA. .125 IN.  
PACKING TORQUE 776 IN.LBS.  
DIRECTION Upward  
GAGE DIA. 11.703 IN.  
SEAL TORQUE 1183 IN.LBS

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



CONTROL SYSTEM ANALYSIS

VALVE SIZE=12		VALVE CLASS=150			FLOW-GAS
UPSTREAM PRESSURE	INITIAL DENSITY-X10 <sup>-2</sup>	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE	
59.7	20.1	340	14.7	59.7	

MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR	
AIR	1.4	1	1	290 SEC	761

STEM DIA.	CAGE DIA.	PACKING TORQUE	SEAL TORQUE	
1.25	11.703	756	1183	

STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	12.0	0.0	0.500	0.50000
2	VALVE	12.0	0.0	0.759	0.75903
3	STRAIGHT PIPE	12.0	11.0	0.165	0.16500
4	VALVE	12.0	0.0	0.759	0.75903
5	EXIT	12.0	0.0	1.000	1.00000

FLOW IN NONPREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN

FLOW = 3,317.47 SCFM

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	471.4
2	53.3	0.1855	329.2	509.4
3	48.5	0.1732	320.4	545.4
4	46.1	0.1673	319.7	583.2
5	40.2	0.1516	303.6	624.9
6	14.7	0.0738	227.8	1282.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT

VALVE TORQUE = 2,542 IN. LBS  
DELTA P = 45.00 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	3,527,149	5.75	4,435
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	53.3	0.1895	329.2
3	48.5	0.1732	320.4
4	46.1	0.1673	315.9
5	40.2	0.1516	303.6
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	3,517,149	11.89	956
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	53.3	0.1895	329.2
3	48.5	0.1732	320.4
4	46.1	0.1673	315.9
5	31.5	0.1352	290.0
6	14.7	0.0733	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	3,099,067	18.46	- 207
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	55.0	0.1896	332.2
3	51.5	0.1812	323.1
4	50.0	0.1773	323.3
5	31.6	0.1276	293.4
6	14.7	0.0733	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	2,398,102	31.50	491
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.2	0.1950	335.9
3	55.3	0.1904	332.7
4	54.6	0.1866	331.1
5	23.0	0.1019	259.0
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	1,788,061	38.46	997
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0



3	57.4	0.1953	335.5	145.6
4	57.1	0.1949	335.9	246.3
5	18.7	0.0377	244.0	547.0
6	14.7	0.0738	227.8	552.1

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
40	1,214,165	42.37	1,142
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.2	0.2000	339.3
3	58.8	0.1989	338.3
4	58.7	0.1987	338.4
5	16.3	0.0797	234.9
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
30	780,798	44.07	1,137
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2007	339.8
3	59.4	0.2003	339.5
4	57.3	0.2002	337.4
5	15.3	0.0760	230.4
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	377,992	44.76	1,206
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.6	0.2007	337.7
3	59.6	0.2008	339.8
4	59.6	0.2008	339.8
5	14.3	0.0744	228.4
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	191,090	44.94	1,209
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2009	339.9
3	57.3	0.2007	337.7
4	59.6	0.2009	339.9
5	14.7	0.0740	227.9
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 4A

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: Bell & Gossett N721C - SR80 - M3 H4

UPSTREAM PRESSURE 59.7 PSIA      INITIAL DENSITY .201 LBS/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA A  
RATIO OF SP. HEAT 1.4  
COMPRESSIBILITY 1      SPECIFIC GRAVITY 1  
HYDRODYNAMIC FACTOR  
@ 90 DEG 761 IN.LBS  
PSI

STEM DIA. 1.25 IN.  
PACKING TORQUE 756 IN.LBS.  
DIRECTION Preferred      GAGE DIA. 11.703 IN  
SEAL TORQUE 1183 IN.LBS

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



**CONTROL SYSTEM ANALYSIS**

VALVE OPENED      VALVE CLOSED      FLOW DIRECTION

UPSTREAM PRESSURE	INITIAL DENSITY X10 <sup>-2</sup>	INITIAL TEMPERATURE	FINAL PRESSURE	SHUT-OFF PRESSURE
59.7	20.1	340	14.7	59.7

MEDIUM	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDROSTATIC PRESSURE
AIR	1.4	1	1	890 DEG 761

STEM DIA.	GAGE DIA.	PACKING TORQUE	SEAL TORQUE
.125	.11700	453	1190

STATION NO.	TYPE OF RESISTANCE	DIAMETER (IN)	LENGTH (L)	RESISTANCE (X)	CORRECTED RESISTANCE (X)
1	ENTRANCE	12.0	0.0	0.500	0.50000
2	VALVE	12.0	0.0	0.759	0.75903
3	Straight Pipe	12.0	7.2	0.135	0.13500
4	PIPE BEND	12.0	0.0	0.160	0.16000
5	Straight Pipe	12.0	4.0	0.040	0.04000
6	VALVE	12.0	0.0	0.757	0.75703
7	EXIT	12.0	0.0	1.000	1.00000

FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN

FLOW = 3,443,784 SCFM

PRESSURE	DENSITY	TEMPERATURE	VELOCITY
59.7	0.1910	340.0	461.7
53.3	0.1861	329.7	497.4
49.0	0.1746	321.3	530.2
47.7	0.1702	318.2	542.1
45.1	0.1647	313.9	559.1
44.4	0.1629	312.5	564.2
38.4	0.1487	279.3	331.3
34.7	0.0738	227.8	1256.0

NOTE: THERE IS SHOCKED FLOW AT STATION 7

CONDITIONS WITH VALVE SHUT

VALVE TORQUE = 2,242 IN. LBS  
DELTA P = 45.00 PSI



CONDITIONS AS VALVE CLOSES

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
			- 0.540	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	461.5
2	53.6	0.1861	329.7	497.4
3	49.0	0.1746	321.3	530.2
4	47.2	0.1703	319.1	548.7
5	45.1	0.1647	313.9	559.1
6	44.4	0.1629	312.5	564.2
7	39.4	0.1467	299.3	631.5
8	14.7	0.0738	227.8	1256.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	3,443,764	7.92	- 3,330	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	461.5
2	53.6	0.1861	329.7	497.4
3	45.7	0.1533	318.1	536.7
4	43.2	0.1614	311.4	572.2
5	41.5	0.1550	306.4	594.3
6	40.7	0.1582	301.9	609.1
7	33.7	0.1336	288.3	694.0
8	14.7	0.0738	227.8	1256.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
70	3,138,455	12.70	- 1,968	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	420.6
2	54.7	0.1773	332.1	446.0
3	42.2	0.1571	308.1	536.8
4	40.8	0.1531	304.9	549.0
5	38.7	0.1482	300.2	555.3
6	38.4	0.1467	299.8	569.5
7	32.5	0.1301	285.7	642.0
8	14.7	0.0738	221.2	1092.3

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
60	2,494,027	22.72	- 321	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	334.2
2	57.0	0.1945	335.5	344.5
3	47.3	0.1583	290.2	494.7
4	33.4	0.1329	288.1	502.4
5	29.2	0.1178	285.2	570.0
6	28.5	0.1171	282.2	573.3
7	24.0	0.1050	262.2	639.8
8	14.7	0.0738	227.8	909.6

NOTE: THERE IS CHOKED FLOW AT STATION 2



ANGLE 50	FLOW 1,803,874	DP ACROSS VALVE 38.32	Tclosinq 450	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	244.4
2	59.1	0.2009	337.7	237.8
3	52.0	0.0927	285.8	497.4
4	31.5	0.0970	254.0	505.5
5	20.8	0.0748	231.7	518.2
6	20.6	0.0940	250.9	522.3
7	18.8	0.0883	244.7	556.0
8	14.7	0.0733	227.3	555.2

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE 40	FLOW 1,223,954	DP ACROSS VALVE 41.49	Tclosinq 753	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	164.4
2	59.2	0.2000	339.3	164.8
3	17.7	0.0846	240.5	370.3
4	17.5	0.0837	237.7	393.7
5	17.3	0.0829	238.6	398.2
6	17.2	0.0826	238.3	399.6
7	13.4	0.0777	233.1	413.3
8	14.7	0.0738	227.3	447.4

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE 30	FLOW 748,829	DP ACROSS VALVE 43.78	Tclosinq 872	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	100.3
2	59.5	0.2007	339.9	100.3
3	15.3	0.0778	231.8	237.2
4	15.7	0.0775	232.2	260.1
5	15.6	0.0772	231.9	261.2
6	15.3	0.0770	231.7	231.3
7	15.3	0.0760	230.4	265.2
8	14.7	0.0738	227.8	273.1

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE 20	FLOW 378,417	DP ACROSS VALVE 44.62	Tclosinq 902	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	50.7
2	59.3	0.2009	339.9	50.7
3	15.0	0.0751	229.3	135.7
4	15.0	0.0750	229.2	135.8
5	15.0	0.0749	229.1	136.0
6	14.9	0.0749	229.1	136.0
7	14.9	0.0744	228.4	137.0
8	14.7	0.0730	227.0	136.0

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Tclosinq



	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	34.7	0.2020	340.0	69.3
2	59.4	0.2009	339.9	69.3
3	14.7	0.0741	229.2	69.4
4	14.7	0.0741	229.7	69.4
5	14.7	0.0741	229.1	69.5
6	14.7	0.0741	228.1	69.5
7	14.7	0.0740	227.1	69.5
8	14.7	0.0738	227.9	69.7

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATED THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 4B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 12"

VALVE CLASS: 150

ACTUATOR: Bellis N721 C-SR80 - M3HW

UPSTREAM PRESSURE 59.7 PSIA

INITIAL DENSITY .201 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 340 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA AIR

RATIO OF SP. HEAT 1.4

SPECIFIC GRAVITY 1

COMPRESSIBILITY 1

HYDRODYNAMIC FACTOR

@ 90 DEG 701 IN.LBS

PSI

STEM DIA. 1.25 IN.

GAGE DIA. 11.703 IN

PACKING TORQUE 751 IN.LBS.

SEAL TORQUE 1183 IN.LBS

DIRECTION Non-directional

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONTINUOUS SYSTEM ANALYSIS

VALVE SIZE=12

VALVE CLASS#150

FLOW-GAS

UPSTREAM PRESSURE 59.7	INITIAL DENSITY-X10 <sup>+2</sup> 20.1	INITIAL TEMPERATURE 340	FINAL PRESSURE 14.7	SHUT-OFF PRESSURE 59.7
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MEDIA	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	270 SEC

STEM DIA. 1.25	CASE DIA. 11.703	PACKING TORQUE 756	SEAL TORQUE 1193
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STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	12.0	0.0	0.500	0.50000
2	VALVE	12.0	0.0	0.759	0.75903
3	STRAIGHT PIPE	12.0	9.0	0.135	0.13500
4	PIPE BEND	12.0	0.0	0.130	0.13000
5	STRAIGHT PIPE	12.0	4.0	0.060	0.06000
6	VALVE	12.0	0.0	0.759	0.75903
7	EXIT	12.0	0.0	1.000	1.00000

## FLOW IN NONPREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN  
FLOW= 3,443,764 SCFH

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	461.5
2	53.6	0.1351	327.7	477.4
3	49.0	0.1746	321.3	530.2
4	47.2	0.1702	318.1	542.7
5	45.1	0.1647	313.7	559.1
6	44.4	0.1628	312.5	564.2
7	38.4	0.1469	299.8	631.5
8	14.7	0.0738	227.3	1268.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE= 2,542 IN. LBS  
DELTA P = 5.30 PSI



**CONDITIONS AS VALVE CLOSES**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	3,443,.54	5.9	4745
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2010	340.0	461.5
2 53.6	0.1961	329.7	497.4
3 49.0	0.1746	321.3	530.2
4 47.2	0.1702	318.1	542.7
5 45.1	0.1647	313.9	559.1
6 44.4	0.1529	312.5	564.2
7 38.4	0.1489	299.3	531.8
8 14.7	0.0738	227.8	1256.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
80	3,443,764	12.44	964
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2010	340.0	461.5
2 53.6	0.1961	329.7	497.4
3 49.0	0.1746	321.3	530.2
4 47.2	0.1702	318.1	542.7
5 45.1	0.1647	313.9	559.1
6 44.4	0.1523	312.5	564.2
7 32.0	0.1288	234.5	720.1
8 14.7	0.0738	227.8	1256.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
70	3,049,241	17.33	130
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2010	340.0	408.6
2 55.2	0.1901	332.5	431.1
3 51.9	0.1819	326.6	450.7
4 50.7	0.1790	324.6	457.0
5 49.3	0.1755	322.0	454.9
6 49.0	0.1746	321.3	466.1
7 31.6	0.1278	283.7	542.5
8 14.7	0.0738	227.8	1222.1

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
50	2,373,062	31.29	495
PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1 59.7	0.2010	340.0	318.4
2 57.2	0.1951	335.9	327.4
3 55.4	0.1906	332.8	335.1
4 54.3	0.1873	331.7	335.3
5 54.2	0.1878	330.8	338.6
6 54.1	0.1874	330.6	338.6
7 22.8	0.1012	239.4	334.0
8 14.7	0.0738	227.8	866.6

NOTE: THERE IS CHOKED FLOW AT STATION 1



ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
50	1,794,842	39.36	996	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	239.2
2	58.4	0.1990	339.0	242.2
3	57.5	0.1993	338.3	245.1
4	57.3	0.1992	338.0	245.2
5	57.1	0.1947	335.7	246.2
6	57.0	0.1948	335.3	245.1
7	18.6	0.0876	243.9	548.3
8	14.7	0.0733	227.8	650.9

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
40	1,211,947	42.27	1,141	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	162.4
2	59.1	0.2000	337.3	162.3
3	58.3	0.1989	338.6	163.7
4	58.7	0.1997	338.4	163.7
5	58.3	0.1933	338.3	163.7
6	58.6	0.1984	338.2	163.7
7	16.3	0.0797	234.9	409.2
8	14.7	0.0733	227.8	442.0

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
30	749,136	44.03	1,187	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	100.4
2	59.5	0.2007	339.3	100.4
3	59.4	0.2003	339.5	100.6
4	57.3	0.2002	339.3	100.6
5	59.3	0.2001	339.4	100.6
6	59.3	0.2001	339.4	100.6
7	15.3	0.0730	230.4	285.4
8	14.7	0.0733	227.8	273.3

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
20	377,317	44.75	1,206	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	50.5
2	59.6	0.2009	339.9	50.5
3	57.8	0.2008	339.8	50.5
4	59.6	0.2008	339.8	50.5
5	59.6	0.2007	339.8	50.5
6	59.3	0.2397	339.3	50.5
7	14.8	0.0744	228.4	136.6
8	14.7	0.0738	227.8	137.6

NOTE: THERE IS CHOKED FLOW AT STATION 6



ANGLE TO	FLOW 190.753	OF ACROSS VALVE 44.93	CLOSING 1,234	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	25.5
2	59.5	0.2009	339.9	25.5
3	59.5	0.2009	339.9	25.5
4	59.5	0.2009	339.9	25.5
5	59.5	0.2009	339.9	25.5
6	59.5	0.2009	339.9	25.5
7	14.7	0.0740	227.9	69.4
8	14.7	0.0739	227.9	69.5

NOTE: THERE IS CHOKED FLOW AT STATION 6

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 1B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"

VALVE CLASS: 150

ACTUATOR: R. & L. N721C-SR80-M344

UPSTREAM PRESSURE 59.7 PSIA

INITIAL DENSITY ,201 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 340 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA Air

RATIO OF SP. HEAT 1.4

SPECIFIC GRAVITY 1.0

COMPRESSIBILITY 1

HYDRODYNAMIC FACTOR  
@ 90 DEG 118.2 IN.LBS

PSI

STEM DIA. 1.375 IN.

GAGE DIA. 12.974 IN

PACKING TORQUE 832 IN.LBS.

SEAL TORQUE 1454 IN.LBS

DIRECTION Preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



COMPUTATION OF FRICTION HEAD AND FLOW				
VALVE SIZE-1"		VALVE CLASS-150		FLOW-GAS
UPSTREAM DENSITY-LB/FT <sup>3</sup>	INITIAL TEMPERATURE- <sup>°</sup> F	INITIAL TEMPERATURE	FINAL PRESSURE	FINAL PRESSURE
1.00	340	140	140	140
MEDIA	RATIO OF SP. HEAT	SPECIFIC HEAT	COMPRESSIBILITY	HYDRODYNAMIC FACTOR
AIR	1.4	1	1	1.00000
STEM DIA.	DIA.	PACKING TORQUE	SEAL TORQUE	
1.375	12.974	832	1454	
STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	CORRECTED RESISTANCE-(K)
1	ENDLOSS	14.0	0.0	0.300
2	VALVE	14.0	0.0	0.950
3	STRAIGHT PIPE	14.0	11.0	0.141
4	PIPE	14.0	0.0	0.030
5	EXIT	14.0	0.0	1.000

FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN

FL=0.727, L=7.75 FT

PRESSURE	DENSITY	TEMPERATURE	VELOCITY
59.7	0.2019	340.0	485.4
53.5	0.1860	329.6	501.6
48.0	0.1722	319.6	541.9
44.1	0.1570	315.7	585.4
39.2	0.1489	301.5	629.1
14.7	0.0733	227.3	1266.3

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT

VALVE TORQUE= 3,101 IN. LBS  
DELTA P=45.00 PSI



**CONDITIONS AS VALVE CLOSING**

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	446.1
2	53.5	0.1956	336.3	501.5
3	49.0	0.1754	321.9	541.9
4	45.1	0.1672	313.7	553.7
5	39.3	0.1489	301.5	528.1
6	14.7	0.0738	227.8	1266.0

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
80	4,530.955	11.10	- 6,519	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	446.1
2	51.1	0.1675	337.7	577.0
3	49.3	0.1754	321.9	510.1
4	47.6	0.1710	313.7	522.0
5	36.5	0.1416	295.7	533.0
6	14.7	0.0738	227.8	1214.1

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
70	4,030.437	20.69	- 3,992	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	396.8
2	55.6	0.1910	333.1	416.5
3	52.0	0.1754	321.9	438.7
4	50.9	0.1793	324.8	442.8
5	30.2	0.1235	279.8	545.5
6	14.7	0.0738	227.8	1077.7

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
60	3,000.612	33.14	716	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	393.7
2	57.5	0.1956	336.3	311.6
3	55.5	0.1910	333.1	319.3
4	53.0	0.1754	321.9	320.7
5	21.9	0.0982	255.3	621.7
6	14.7	0.0738	227.8	927.0

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
50	2,302.002	39.28	737	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	226.6



1	59.2	0.2001	338.3	131.3
2	59.2	0.2001	339.3	131.3
3	14.7	0.0738	227.8	61.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
40	1,551,983	42.64	1,218
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.3	0.2001	339.4
3	59.2	0.2001	339.3
4	59.3	0.1989	338.5
5	15.1	0.0790	234.1
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
30	951,302	44.15	1,373
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.4	0.2007	339.8
3	59.4	0.2003	339.5
4	59.4	0.2002	339.5
5	15.2	0.0757	230.1
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
20	483,477	44.79	1,436
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.4	0.2007	339.8
3	59.4	0.2003	339.5
4	59.4	0.2002	339.5
5	15.2	0.0757	230.1
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
10	244,414	44.94	1,445
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2007	339.9
3	59.6	0.2004	339.9
4	59.6	0.2009	339.9
5	14.7	0.0739	227.9
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 2B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 14"

VALVE CLASS: 150

ACTUATOR: Bell, N721C-SR80 - M3HW

UPSTREAM PRESSURE 39.7 PSIA

INITIAL DENSITY .201 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 340 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA Air

RATIO OF SP. HEAT 1.4

SPECIFIC GRAVITY 1

COMPRESSIBILITY i

HYDRODYNAMIC FACTOR

@ 90 DEG 1182 IN.LBS  
PSI

STEM DIA. 1.375 IN.

GAGE DIA. 12.974 IN

PACKING TORQUE 832 IN.LBS.

SEAL TORQUE 1454 IN.LBS

DIRECTION Preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONTROL SYSTEM ANALYSIS

VALVE SIZE-14		VALVE CLASS-150			FLOW-GAS
STREAM PRESSURE PSI	INITIAL DENSITY- LB/SCF	INITIAL TEMPERATURE °F	FINAL PRESSURE PSI	SHUT-OFF PRESSURE PSI	

MEDIA	RATIO OF SP. WT.	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR	
AIR	1.4	1	1	1182	

STEM DIA. 1.375	CHOKING DIA. 12.974	PACKING TORQUE 932	2916 TORQUE 1454	
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STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	14.0	0.0	0.500	0.50000
2	VALVE	14.0	0.0	0.960	0.96065
3	STRAIGHT PIPE	14.0	9.0	0.115	0.11571
4	PIPE BEND	14.0	0.0	0.130	0.13000
5	STRAIGHT PIPE	14.0	3.0	0.038	0.03857
6	VALVE	14.0	0.0	0.860	0.86065
7	EXIT	14.0	0.0	1.000	1.00000

## FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN  
FLOW= 4,645,997 SCFH

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY	
1	59.7	0.2010	340.0	457.5	
2	58.7	0.1383	330.0	421.7	
3	48.5	0.1734	320.0	528.9	
4	47.2	0.1599	317.0	539.2	
5	43.1	0.1645	313.0	554.3	
6	44.7	0.1636	313.1	556.2	
7	37.8	0.1450	298.4	633.9	
8	14.0	0.0733	227.0	1077.7	

NOTE: THERE IS CHOKED FLOW AT STATION 7

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE= 3,101 IN. LBS  
DELTAP= 13.00 PSI



CONDITIONS AS VALVE CLOSING

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
			- 33	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	440.1
2	53.7	0.1966	330.0	491.7
3	48.5	0.1934	320.5	529.9
4	44.2	0.1903	311.3	539.0
5	45.1	0.1848	313.9	554.5
6	44.7	0.1836	313.1	556.2
7	35.2	0.1830	293.7	333.3
8	14.7	0.0738	227.8	1244.7

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	80	4,467,262	11.29	- 6,516
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	440.1
2	54.3	0.1980	331.0	469.3
3	47.7	0.1733	322.8	500.4
4	48.5	0.1733	320.4	507.6
5	46.6	0.1685	316.8	521.2
6	48.4	0.1530	315.3	522.2
7	35.1	0.1377	292.1	642.2
8	14.7	0.0738	227.8	1197.7

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	70	3,982,960	20.51	- 3,754
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	392.1
2	53.3	0.1711	333.1	411.3
3	52.2	0.1927	327.2	430.7
4	51.4	0.1907	325.8	434.2
5	50.2	0.1777	323.5	440.3
6	50.1	0.1774	323.4	440.3
7	29.4	0.1217	273.2	647.2
8	14.7	0.0738	227.8	1067.2

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	60	3,040,321	32.73	- 730
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	361.1
2	57.6	0.1960	336.5	309.0
3	55.7	0.1914	333.4	316.3
4	55.1	0.1903	332.8	317.5
5	54.3	0.1892	331.8	318.9
6	54.7	0.1890	331.7	318.9
7	21.3	0.0737	265.3	527.7
8	14.7	0.0738	227.8	322.1

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4

1



5



ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
40	2,038.348	39.15	791.6777	
PRESSURE DENSITY TEMPERATURE VELOCITY				
1	59.7	0.2010	340.0	125.3
2	59.6	0.2009	339.3	127.3
3	59.3	0.2001	339.3	130.1
4	59.5	0.1998	338.4	130.4
5	59.3	0.1993	338.1	130.4
6	59.3	0.1782	338.0	130.4
7	18.1	0.0859	242.0	525.3
8	14.7	0.0738	227.8	613.2

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
40	1,551,568	42.55	1,217	
PRESSURE DENSITY TEMPERATURE VELOCITY				
1	59.7	0.2010	340.0	152.7
2	59.3	0.2001	339.4	153.1
3	59.3	0.1990	338.6	153.9
4	59.2	0.1989	338.5	153.9
5	59.7	0.1787	338.4	153.7
6	58.7	0.1986	338.4	153.9
7	16.1	0.0790	234.1	388.3
8	14.7	0.0738	227.3	413.7

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
30	753,471	44.13	1,373	
PRESSURE DENSITY TEMPERATURE VELOCITY				
1	59.7	0.2010	340.0	94.3
2	59.6	0.2007	339.8	94.3
3	59.4	0.2003	339.5	94.5
4	59.4	0.1993	339.2	94.5
5	59.3	0.2002	339.4	94.5
6	59.3	0.2002	339.4	94.5
7	18.1	0.0797	230.1	250.3
8	14.7	0.0738	227.8	256.3

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
20	482,546	44.78	1,436	
PRESSURE DENSITY TEMPERATURE VELOCITY				
1	59.7	0.2010	340.0	47.5
2	59.6	0.2009	339.7	47.5
3	59.3	0.2003	339.3	47.5
4	59.6	0.2008	339.3	47.5
5	59.6	0.2008	339.3	47.5
6	59.3	0.2003	339.4	47.5
7	14.8	0.0743	228.3	129.4
8	14.7	0.0738	227.9	129.3

NOTE: THERE IS CHOKED FLOW AT STATION 6



	143.840	143.840	143.840	143.840
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	52.7	0.2010	340.0	24.0
2	59.3	0.1963	339.9	24.1
3	64.0	0.1909	339.9	24.1
4	59.3	0.2019	339.9	24.0
5	59.3	0.2003	334.4	24.0
6	59.3	0.2009	339.9	24.0
7	14.7	0.0739	227.9	55.2
8	14.7	0.0739	227.9	55.3

NOTE: THERE IS CHOKED FLOW AT STATION 6

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 3A

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 12"

VALVE CLASS: 150

ACTUATOR: Bell & Gossett - N721C - SK80 - M3H4

UPSTREAM PRESSURE 59.7 PSIA

INITIAL DENSITY .201 LBS/FT<sup>3</sup>

INITIAL TEMPERATURE 340 °F

FINAL PRESSURE 14.7 PSIA

SHUT OFF PRESSURE 59.7 PSIA

MEDIA Air

RATIO OF SP. HEAT 1.4

SPECIFIC GRAVITY 1

COMPRESSIBILITY 1

HYDRODYNAMIC FACTOR  
@ 90 DEG 761 EN.LBS

PSI

STEM DIA. 1.25 IN.

GAGE DIA. 11.703 IN

PACKING TORQUE 757 IN.LBS.

SEAL TORQUE 1183 IN.LBS

DIRECTION Parallel

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)

B.CI



WATER FLOW THROUGH A VALVE					FLOW-RATE
VALVE SIZE-10		VALVE CLASS=150			FLOW-RATE
UPSTREAM PRESSURE	INITIAL DENSITY- $\times 10^{-3}$	INITIAL TEMPERATURE	FINAL PRESSURE	INITIAL PRESSURE	
psi	lb/in <sup>2</sup>	°F	psi	lb/in <sup>2</sup>	
MEDIUM	RATIO OF SP. HEAT	SPECIFIC GRAVITY	COMPRESSIBILITY	HYDRODYNAMIC FACTOR	
AIR	1.4	1	1	1.00	761
STEM DIA.	GAGE DIA.	LOADING TORQUE	LEAK TORQUE		
1.25	.11.703	756	1183		
STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	RESISTANCE-(K)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	12.0	0.0	0.000	0.0000
2	VALVE	12.0	0.0	0.759	0.75903
3	STRAIGHT PIPE	12.0	11.0	0.165	0.16500
4	CHOKING	12.0	0.0	0.750	0.75007
5	EXIT	12.0	0.0	1.000	1.00000
FLOW IN PREFERRED DIRECTION					
CONDITIONS WITH VALVE OPEN					
FLOW = 3.007, 17 SCFM					
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY	
1	52.7	0.12910	340.0	714.4	
2	53.3	0.12855	329.2	509.4	
3	48.5	0.1732	320.4	545.4	
4	48.1	2.1073	319.7	333.2	
5	40.2	0.1515	303.6	524.9	
6	14.7	0.0738	227.3	1222.7	

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT  
 VALVE TORQUE = 2,542 IN. LBS  
 DELTA P=45.00 PSI



## CONDITIONS AT VALVE 1

ANGLE	FLOW	DP ACROSS VALVE	Telesing
		1.25	100%
1	59.7	0.2010	340.0
2	53.3	0.1955	329.2
3	48.5	0.1732	320.4
4	45.7	0.1573	313.7
5	40.2	0.1518	303.6
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Telesing
30	3,517,149	9.39	- 3,237
1	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	53.3	0.1955	327.1
3	44.9	0.1641	313.5
4	42.3	0.1573	308.2
5	35.4	0.1394	272.7
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Telesing
70	3,179,985	13.52	- 1,773
1	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	54.2	0.1890	331.7
3	41.2	0.1544	305.7
4	39.2	0.1490	301.6
5	33.3	0.1326	287.3
6	14.7	0.0738	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE	FLOW	DP ACROSS VALVE	Telesing
30	2,474,313	27.24	- 201
1	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.0	0.1945	335.5
3	29.0	0.1202	276.3
4	27.7	0.1193	273.2
5	24.0	0.1050	262.2
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	Telesing
50	1,923,803	37.17	758
1	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0

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ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
40	1,223,314	41.80	1,058

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
40	1,223,314	41.80	1,058
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.2	0.2000	339.3
3	57.4	0.0735	239.1
4	17.2	0.0826	238.3
5	16.4	0.0799	235.1
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
30	743,310	43.83	1,173

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
30	743,310	43.83	1,173
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2007	339.3
3	15.7	0.0774	232.1
4	15.2	0.0770	231.7
5	15.3	0.0760	230.4
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
20	373,407	44.85	1,202

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
20	373,407	44.85	1,202
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	57.3	0.2003	337.7
3	15.0	0.0750	229.2
4	14.7	0.0749	229.1
5	14.3	0.0744	228.4
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
10	191,313	44.91	1,209

ANGLE	FLOW	DP ACROSS VALVE	T <sub>closing</sub>
10	191,313	44.91	1,209
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.3	0.2009	339.9
3	14.7	0.0741	229.1
4	14.7	0.0741	229.1
5	14.7	0.0740	227.9
6	14.7	0.0738	227.3

NOTE: THERE IS CHOKED FLOW AT STATION 2

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN

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CASE 3B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 1/2"  
VALVE CLASS: 150  
ACTUATOR: Bell, N771C-SN80-M3HW

UPSTREAM PRESSURE 57.7 PSIA      INITIAL DENSITY .201 LBS/FT<sup>3</sup>  
INITIAL TEMPERATURE 340 °F      FINAL PRESSURE 14.7 PSIA  
SHUT OFF PRESSURE 59.7 PSIA      MEDIA Air  
RATIO OF SP. HEAT 1.4      SPECIFIC GRAVITY 1  
COMPRESSIBILITY 1      HYDRODYNAMIC FACTOR  
@ 90 DEG 761 IN.LBS  
                                          PSI

STEM DIA. 1.25 IN.      GAGE DIA. 1.703 IN  
PACKING TORQUE 756 IN.LBS.      SEAL TORQUE 1183 IN.LBS  
DIRECTION Preferred

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)

*B65*



VALVE SIZE=10		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE 39.7	INITIAL DENSITY-1010 20.7	INITIAL TEMPERATURE 340	FINAL PRESSURE 14.7	SHUT-OFF PRESSURE 37.7
MEDIA AIR	RATIO OF SP. WT. 1.4	SPECIFIC GRAVITY 1	COMPRESSIBILITY 1.00000	HYDRODYNAMIC FACTOR 761
STEM DIA. 1.25	ODS 11.703	TORQUE 756	SEAL TORQUE 1183	
STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	UNPRESSED RESISTANCE-(K)
1	ENTRANCE	12.0	0.0	0.300
2	VALVE	12.0	0.0	0.759
3	STRAIGHT PIPE	12.0	11.0	0.135
4	VALVE	12.0	0.0	0.757
5	EXIT	12.0	0.0	1.000
				RESISTANCE-(K)

FLOW IN REVERSED DIRECTION

CONDITIONS WITH VALVE OPEN

FLOW 3,317,147 SCFM

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	39.7	0.2010	340.0	472.4
2	53.3	0.1855	329.2	509.4
3	48.5	0.1732	320.4	545.4
4	43.1	0.1573	313.7	583.2
5	40.2	0.1516	303.6	624.9
6	14.7	0.0738	227.8	1232.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE = 2,542 IN. LBS  
DELTA P=45.00 PSI



## CONDUIT LINES AS VALVE CLOSURES

ANGLE 90	FLOW 3,517,149	DP ACROSS VALVE 11.89	Tclosing - 4,100	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	471.4
2	53.3	0.1655	329.2	509.4
3	48.5	0.1732	320.4	545.4
4	46.1	0.1673	315.9	563.2
5	40.2	0.1518	303.9	524.9
6	14.7	0.0738	227.9	1292.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE 90	FLOW 3,517,149	DP ACROSS VALVE 11.89	Tclosing - 4,100	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	471.4
2	53.3	0.1638	327.2	507.4
3	48.5	0.1732	320.4	545.4
4	46.1	0.1673	315.9	563.2
5	34.2	0.1392	296.0	700.3
6	14.7	0.0738	227.9	1292.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE 70	FLOW 3,099,037	DP ACROSS VALVE 18.46	Tclosing - 2,135	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	415.3
2	55.0	0.1396	332.2	439.4
3	51.3	0.1321	323.1	460.3
4	50.0	0.1773	323.3	469.0
5	31.3	0.1278	293.4	653.9
6	14.7	0.0738	227.9	1292.7

NOTE: THERE IS CHOKED FLOW AT STATION 5

ANGLE 60	FLOW 3,074,102	DP ACROSS VALVE 31.59	Tclosing - 187	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	321.1
2	57.2	0.1950	335.9	330.1
3	55.3	0.1904	332.7	338.1
4	54.3	0.1393	321.4	340.3
5	23.0	0.1018	259.0	633.9
6	14.7	0.0738	227.9	1292.7

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE 50	FLOW 1,788,061	DP ACROSS VALVE 38.46	Tclosing 751	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	239.3



ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	191,090	44.94	1,209

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
40	1,214,185	42.37	1,059
	AVERAGE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.2	0.2000	339.3
3	59.3	0.2009	339.3
4	58.7	0.1987	338.4
5	15.3	0.0797	234.9
6	14.7	0.0733	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	360,780	44.67	1,174
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.5	0.2007	339.3
3	59.4	0.2003	339.3
4	59.3	0.2002	339.3
5	15.3	0.0760	230.4
6	14.7	0.0733	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
20	377,992	44.76	1,203
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.3	0.2007	339.3
3	59.6	0.2009	339.3
4	59.5	0.2008	339.3
5	14.5	0.0744	230.4
6	14.7	0.0733	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4.

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
10	191,090	44.94	1,209
	PRESSURE	DENSITY	TEMPERATURE
1	59.7	0.2010	340.0
2	59.6	0.2009	339.3
3	59.6	0.2009	339.3
4	59.5	0.2009	339.3
5	14.7	0.0740	230.4
6	14.7	0.0733	227.8

NOTE: THERE IS CHOKED FLOW AT STATION 4

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN



CASE 4B

CONDITION 2

NUCLEAR LOCA ANALYSIS

VALVE SIZE: 12"

VALVE CLASS: 150

ACTUATOR: Delti, N721 C - CRYO - M3HW

UPSTREAM PRESSURE 59.7 PSIA

INITIAL TEMPERATURE 340 °F

SHUT OFF PRESSURE 59.7 PSIA

RATIO OF SP. HEAT 1.4

COMPRESSIBILITY 1

INITIAL DENSITY .201 LBS/FT<sup>3</sup>

FINAL PRESSURE 14.7 PSIA

MEDIA Ai

SPECIFIC GRAVITY 1

HYDRODYNAMIC FACTOR

@ 90 DEG 761 IN.LBS  
PSI

STEM DIA. 1.25 IN.

GAGE DIA. 11.703 IN

PACKING TORQUE 756 IN.LBS.

SEAL TORQUE 1183 IN.LBS

DIRECTION Procedural

INPUT STATION NO., K FACTORS, ETC.

(See Appendix A)



## CONVENTIONAL STATION ANALYSIS

VALVE SIZE=12		VALVE CLASS=150		FLOW-GAS
UPSTREAM PRESSURE 59.7	INITIAL DENSITY=0.2010	INITIAL TEMPERATURE 340	FINAL PRESSURE 59.7	SHUT-OFF PRESSURE 59.7
MEDIA AIR	RATIO OF SPC. HEAT 1.4	SPECIFIC CAPACITY 1	COMPRESSIBILITY 1	HYDRODYNAMIC FACTOR 0.70 SEC 761
STEM DIA. 1.125	PIPE DIA. 11.703	PACKING TORQUE 756	SEAL TORQUE 1183	.
STATION NO.	TYPE OF RESISTANCE	DIAMETER-(D)	LENGTH-(L)	CORRECTED RESISTANCE-(K)
1	ENTRANCE	12.0	0.0	0.300
2	VALVE	12.0	0.0	0.759
3	STRAIGHT PIPE	12.0	9.0	0.135
4	PIPE BEND	12.0	0.0	0.135
5	STRAIGHT PIPE	12.0	4.0	0.060
6	VALVE	12.0	0.0	0.759
7	EXIT	12.0	0.0	1.000
CORRECTED RESISTANCE-(K)				

## FLOW IN PREFERRED DIRECTION

CONDITIONS WITH VALVE OPEN  
FLOW= 3,443,764 SCFH

	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	461.5
2	53.3	0.1932	327.7	477.4
3	49.0	0.1746	321.3	530.2
4	47.2	0.1702	318.1	542.7
5	45.1	0.1547	313.9	557.1
6	44.4	0.1628	312.5	564.3
7	38.4	0.1469	299.3	631.5
8	24.7	0.0733	227.0	1298.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

CONDITIONS WITH VALVE SHUT  
VALVE TORQUE= 2,542 IN. LBS  
SOLUTN P=43.30 PSIG



## CONDITIONS AS VALVE CLOSING

ANGLE	FLOW STATION	DP ACROSS VALVE 1.17	Tclosing	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	461.5
2	53.6	0.1951	329.7	497.4
3	49.0	0.1746	321.3	530.2
4	47.2	0.1702	318.1	542.7
5	45.1	0.1647	313.9	559.1
6	44.4	0.1629	312.5	564.2
7	38.4	0.1589	292.8	534.5
8	14.7	0.0738	227.8	1256.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	80	12.44	- 4,127	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	461.5
2	53.6	0.1951	329.7	497.4
3	49.0	0.1746	321.3	530.2
4	47.2	0.1702	318.1	542.7
5	45.1	0.1647	313.9	559.1
6	44.4	0.1589	312.5	564.2
7	32.0	0.1238	294.5	720.1
8	14.7	0.0738	227.8	1256.0

NOTE: THERE IS CHOKED FLOW AT STATION 7

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	70	17.33	- 2,044	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	403.6
2	53.6	0.1951	329.7	431.6
3	51.9	0.1919	326.3	450.7
4	50.7	0.1790	324.3	457.0
5	47.3	0.1755	321.0	464.3
6	49.0	0.1746	321.3	466.1
7	31.6	0.1278	293.7	643.5
8	14.7	0.0738	227.8	1222.1

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing	
	60	31.29	- 150	
	PRESSURE	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	315.4
2	57.2	0.1951	335.9	327.4
3	55.4	0.1906	332.8	335.1
4	54.3	0.1893	331.7	333.3
5	54.2	0.1878	330.8	338.6
6	54.1	0.1874	330.6	338.5
7	22.3	0.1012	298.4	332.0
8	14.7	0.0738	227.8	866.6



ANGLE	FLOW	DP ACROSS VALVE	Tclosing
1	1.124,342	50.35	751
2			
3			
4			
5			
6			
7			
8			
9			

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
1	1,211.947	42.27	1,059
2			
3			
4			
5			
6			
7			
8			
9			

NOTE: THERE IS CHOKED FLOW AT STATION 6

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
1	747.438	44.03	2,274
2			
3			
4			
5			
6			
7			
8			
9			

NOTE: THERE IS CHOKED FLOW AT STATION 3

ANGLE	FLOW	DP ACROSS VALVE	Tclosing
1	377,317	44.75	1,203
2			
3			
4			
5			
6			
7			
8			
9			

NOTE: THERE IS CHOKED FLOW AT STATION 6



	1.000		1.000	
	STATION	1.000	1.000	
	FREQUENCY	DENSITY	TEMPERATURE	VELOCITY
1	59.7	0.2010	340.0	25.5
2	59.8	0.2009	339.9	25.5
3	59.9	0.2009	339.9	25.5
4	59.8	0.2009	339.9	25.5
5	59.8	0.2009	339.9	25.5
6	59.6	0.2009	339.9	25.5
7	14.7	0.0740	227.9	69.4
8	14.7	0.0739	227.9	69.4

NOTE: THERE IS CHOKED FLOW AT STATION 5

NOTE: A POSITIVE CLOSING TORQUE INDICATES THAT THE VALVE WILL TEND TO REMAIN OPEN

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APPENDIX C

Determination of Closing Times

NOTE: Positive torques are tending to open the valve, negative torques are tending to close the valve.



DETERMINATION OF CLOSING TIME

VALVE SIZE 14" VALVE CLASS 150

ACTUATOR B+L1s N721C-SR80-M3HU

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Perpend.

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 7770

ACTUATOR VOLUME .72 SCF

ACTUATOR PRESSURE 40 PSIG

MEDIA Air

HYDRODYNAMIC TORQUE @ 90 1182

PACKING TORQUE 832 IN.LBS.

STEM DIA. 1.375 IN.

BUILDING PRESSURE 45 PSIG

ACTUATOR YORE RADIUS 2.5 IN.

SOLENOID VALVE C<sub>v</sub> 2.26

VALVE C<sub>v</sub> 6317

SHUT OFF PRESSURE DROP 45 PSI

SEAL TORQUE 1451 IN.LBS.

GAGE DIA. 12.974 IN.

dt .05 SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	.0741	65.2	44.9
20	.0749	127.7	44.7
30	.0770	245.3	44.0
40	.0826	374.9	42.1
50	.0939	492.8	37.9
60	.115	549.5	29.9
70	.151	546.9	15.2
80	.161	579.0	9.74
90	.172	541.9	5.78



**DETERMINATION OF CLOSING TIME**

THE VALVE IS IN THE PREFERRED DIRECTION

Spring常数= 5930  
ACT. VOL.= .72

MODULUS= 10000  
PACKING TORQUE= 932  
BUILDING PRESSURE= 45

Spring angle= 37°  
ACT. YOKE RADIUS= 0.5

YOLK TORQUE= 1454  
SEAL TORQUE= 1454

ACT. PRESS= 90  
Diam.= 1.375

SOL. VALVE C= 0.33  
Shaft diameter, inches= .375  
Diameter= 12.974

DEG.	10	20	30	40	50	60	70	80	90
DENSITY	.0741	.0749	.0773	.0824	.0939	.1159	.1513	.1613	.1720
VELOCITY	65.2	127.7	245.8	374.8	492.8	549.5	546.9	579.0	541.7
PRES DROP	44.90	44.70	44.00	42.10	37.70	29.90	15.20	9.74	5.48

LOCA CLOSES THE VALVE TO 63 DEGREES WITH THE ACTUATOR STILL ACTUATED

MAXIMUM AERODYNAMIC TORQUE AS VALVE CLOSES IS -0032 IN-LBS. AT 90 DEGREES

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	0	4634	-3137	2652	499	614	63.00	25.49
0.05	0	2558	-2843	-928	499	614	52.35	36.01
0.10	0	2048	-2773	-389	499	614	45.34	39.54
0.15	0	1800	-2703	-208	499	614	40.39	41.31
0.20	0	1677	-2673	-112	499	614	36.03	42.35
0.25	0	1623	-2678	-58	499	614	31.71	43.53
0.30	0	1820	-2702	-3	499	614	28.11	44.13
0.35	0	1649	-2745	-17	499	614	24.56	44.39
0.40	0	1701	-2805	-3	499	614	21.21	44.51
0.45	0	1772	-2831	-4	499	614	18.03	44.73
0.50	0	1859	-2970	-2	499	614	15.06	44.79
0.55	0	1959	-3071	-1	499	614	12.24	44.85
0.60	0	2021	-3134	0	499	614	9.97	44.90
0.65	0	2194	-3308	0	499	614	7.09	44.92
0.70	0	2327	-3440	0	499	614	4.75	44.95
0.75	0	2715	-3590	0	100	614	2.25	44.97
0.80	0	1382	-3693	0	1696	614	0.96	44.99



DETERMINATION OF CLOSING TIMEVALVE SIZE 14" VALVE CLASS 150ACTUATOR Bell's N721C-SR80-M3HWAMOUNT OF VALVE OPENING 90°DIRECTION OF FLOW No preference

## ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>40</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>
MEDIA	<u>H2</u>		VALVE C <sub>v</sub>	<u>6317</u>
HYDRODYNAMIC TORQUE @ 90	<u>1182</u>		SHUT OFF PRESSURE DROP	<u>45</u> PSI
PACKING TORQUE	<u>832</u>	IN.LBS.	SEAL TORQUE	<u>1454</u> IN.LBS.
STEM DIA.	<u>1.375</u>	IN.	GAGE DIA.	<u>12.974</u> IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.25</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0739</u>	<u>65.3</u>	<u>44.9</u>
20	<u>.0743</u>	<u>128.7</u>	<u>44.8</u>
30	<u>.0757</u>	<u>250.7</u>	<u>44.2</u>
40	<u>.0790</u>	<u>388.7</u>	<u>42.6</u>
50	<u>.0861</u>	<u>529.0</u>	<u>39.3</u>
60	<u>.0942</u>	<u>661.7</u>	<u>33.1</u>
70	<u>.124</u>	<u>645.5</u>	<u>20.7</u>
80	<u>.142</u>	<u>633.0</u>	<u>11.1</u>
90	<u>.149</u>	<u>628.1</u>	<u>6.92</u>



**DETERMINATION OF CLOSING TIME**

14" 150 CLASS VALVE WITH A RATED DISCHARGE

THE VALVE IS IN THE NON-PREFERRED DIRECTION

Spring begin= 5930      Spring ending 3770  
 ACT. "UL." = .72      ACT. VALVE RADIUS= 0.5  
 MECHANISM =  
 PACKING TORQUE= 932      VALVE CV= 3317  
 SEAL TORQUE= 1454      HYDRO. TORQUE @ 70= .1222  
 BUILDING PRESSURE= 3.1      Stem= 1.375      SHUT-THRU VALVE, S.D.C. = .75

ACT. PRESS= 80

END. VALVE CV= 1.18

SHUT-THRU VALVE, S.D.C. = .75

Dgage= 12.974

DEC.	10	20	30	40	50	60	70	80	90
CENSITY	.0737	.0773	.0797	.0790	.0831	.0932	.11210	.1420	.1420
VELOCITY	55.3	123.7	250.7	398.4	529.0	621.7	645.5	633.6	629.1
PRES DROP	44.90	44.30	44.20	42.60	39.30	33.10	20.70	11.10	6.92

TIME sec	TORQUE torque to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	14946	12993	-5924	6431	832	614	90.00	6.92
0.25	7847	5870	-5924	6431	832	614	90.00	6.92
0.50	3229	4276	-5924	6431	832	614	90.00	6.92
0.75	5436	3483	-5924	6431	832	614	90.00	6.92
1.00	4720	2733	-5924	6431	832	614	90.00	6.92
1.25	4530	2577	-5924	6431	832	614	90.00	6.92
1.50	4242	2289	-5924	6431	832	614	90.00	6.92
1.75	4013	2082	-5924	6431	832	614	90.00	6.92
2.00	3830	1877	-5924	6431	832	614	90.00	6.92
2.25	3670	1724	-5924	6431	832	614	90.00	6.92
2.50	3547	1575	-5924	6431	832	614	90.00	6.92
2.75	3438	1485	-5924	6431	832	614	90.00	6.92
3.00	3342	1389	-5924	6431	832	614	90.00	6.92
3.25	3259	1305	-5924	6431	832	614	90.00	6.92
3.50	3185	1231	-5924	6431	832	614	90.00	6.92
3.75	3112	1166	-5924	6431	832	614	90.00	6.92
4.00	3040	1107	-5924	6431	832	614	90.00	6.92
4.25	3007	1053	-5924	6431	832	614	90.00	6.92
4.50	2959	1005	-5924	6431	832	614	90.00	6.92
4.75	2913	961	-5924	6431	832	614	90.00	6.92
5.00	2875	921	-5924	6431	832	614	90.00	6.92
5.25	2838	884	-5924	6431	832	614	90.00	6.92
5.50	2804	850	-5924	6431	832	614	90.00	6.92
5.75	2772	819	-5924	6431	832	614	90.00	6.92
6.00	2743	790	-5924	6431	832	614	90.00	6.92
6.25	2715	763	-5924	6431	832	614	90.00	6.92
6.50	2691	738	-5924	6431	832	614	90.00	6.92
6.75	2667	714	-5924	6431	832	614	90.00	6.92

c-4



DETERMINATION OF CLOSING TIME

VALVE SIZE 1/4" VALVE CLASS 150

ACTUATOR B.LI., 1721C-SA90

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Per L.

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE $C_v$	<u>2.20</u>
MEDIA	<u>Air</u>		VALVE $C_v$	<u>6.717</u>
HYDRODYNAMIC TORQUE @ 90	<u>118 L</u>		SHUT OFF PRESSURE DROP	<u>4.5</u> PSI
PACKING TORQUE	<u>83 Z</u>	IN.LBS.	SEAL TORQUE	<u>145 Y</u> IN.LBS.
STEM DIA.	<u>1.375</u>	IN.	GAGE DIA.	<u>12.974</u> IN.
BUILDING PRESSURE	<u>45</u>	PSIG	$dt$	<u>.05</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0711</u>	<u>65.7</u>	<u>44.9</u>
20	<u>.0750</u>	<u>128.0</u>	<u>44.7</u>
30	<u>.0774</u>	<u>247.8</u>	<u>43.9</u>
40	<u>.0833</u>	<u>372.8</u>	<u>41.9</u>
50	<u>.0957</u>	<u>483.3</u>	<u>32.4</u>
60	<u>.119</u>	<u>534.0</u>	<u>28.7</u>
70	<u>.153</u>	<u>533.4</u>	<u>14.4</u>
80	<u>.163</u>	<u>521.6</u>	<u>9.13</u>
90	<u>.173</u>	<u>528.9</u>	<u>5.22</u>



DETERMINATION OF CLOSING TIME

THE VALVE IS IN THE PREFERRED DIRECTION

SPRING BEGINS 5970 ACT. VOL. = .0	SPRING ENDING 3770 ACT. VOL. RADIUS = 2.5	ACT. PRESS = 80 HYDRO. TORQUE = 1132 Diameter = 1.375	SOL. VALVE CV = 2.0 SHUT-OFF TIME = 11.92 Dgage = 12.974						
NEUTRAL	VALVE CV = 5.217								
PACKING TORQUE = 932	SEAL TORQUE = 1454								
GUILTING FREASURE = 45									
DEG.	10	20	30	40	50	60	70	80	90
DENSITY	.0741	.0750	.0774	.0833	.0957	.1190	.1630	.1830	.1730
VELOCITY	65.4	128.0	244.9	372.8	483.3	534.0	533.4	561.6	523.9
PRES DROP	44.90	44.70	43.90	41.90	37.40	28.70	14.40	9.13	5.22

LOCA CLOSES THE VALVE TO 63 DEGREES WITH THE ACTUATOR STILL ACTUATED

MAXIMUM AERODYNAMIC TORQUE AS VALVE CLOSES IS -3373 IN-LBS. AT 63 DEGREES

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	0	4834	-3377	2481	499	614	63.00	24.71
0.05	0	2541	-2843	-811	499	614	52.35	35.35
0.10	0	2045	-2773	-385	499	614	45.88	39.25
0.15	0	1802	-2763	-297	499	614	40.31	41.50
0.20	0	1677	-2678	-113	499	614	36.08	42.33
0.25	0	1623	-2678	-58	499	614	31.95	43.50
0.30	0	1817	-2702	-31	499	614	28.15	44.04
0.35	0	1649	-2745	-17	499	614	24.60	44.33
0.40	0	1700	-2805	-9	499	614	21.25	44.59
0.45	0	1771	-2860	-4	499	614	18.00	44.73
0.50	0	1858	-2969	-2	499	614	15.10	44.77
0.55	0	1953	-3070	-1	499	614	12.23	44.85
0.60	0	2070	-3193	-0	499	614	7.92	44.90
0.65	0	2193	-3306	-0	499	614	7.12	44.92
0.70	0	2325	-3439	-0	499	614	4.79	44.95
0.75	0	2723	-3577	-0	1033	614	2.60	44.99
0.80	0	1385	-3693	-0	1593	614	0.97	44.99



DETERMINATION OF CLOSING TIMEVALVE SIZE 14 VALVE CLASS 150ACTUATOR Bell N721C-SR80-MJHWAMOUNT OF VALVE OPENING 90°DIRECTION OF FLOW Upward

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YOKE RADIUS	<u>.25</u>	IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>.226</u>	
MEDIA	<u>A:-</u>		VALVE C <sub>v</sub>	<u>.217</u>	
HYDRODYNAMIC TORQUE @ 90	<u>1182</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>832</u>	IN.LBS.	SEAL TORQUE	<u>1454</u>	IN.LBS.
STEM DIA.	<u>.375</u>	IN.	GAGE DIA.	<u>.12.974</u>	IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.25</u>	SEC.

DEG.	LOCA TORQUE (IN.LBS)
10	<u>1477</u>
20	<u>1565</u>
30	<u>1859</u>
40	<u>2333</u>
50	<u>2786</u>
60	<u>2367</u>
70	<u>1106</u>
80	<u>2170</u>
90	<u>7287</u>



**DETERMINATION OF CLOSING TIME**  
IN A CYLINDER VALVE WITH A METAL SEAT AND SPRINGS

THE VALVE IS IN THE PREFERRED DIRECTION

Spring begins 8930      Starting setting 37°  
 ACT. VOL. = .72      ACT. TORQUE RADIUS = 2.6  
 MEDIA=air      Valve dia = 3.517  
 PACKING TORQUE = 932      SEAL TORQUE = 1454  
 BUILDING PRESSURE = 3.1

ACT. PRESSURE =  
 INTERNAL FORCED = 10.000  
 Stem = 1.375

SOL. VALVE C.D. = 3.05  
 EXTERNAL PRESSURE = 10.000  
 Dgage = 10.974

DEG.	10	20	30	40	50	60	70	80	90
LECA FORMULAE	1477	1665	1963	2333	2791	3357	4103	5170	7237

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees
0.00	14355	12993	-5924	5840	832	614	90.00
0.25	7033	5579	-5924	5840	832	614	90.00
0.50	5633	4276	-5924	5840	832	614	90.00
0.75	4845	3483	-5924	5840	832	614	90.00
1.00	4213	2927	-5924	5840	832	614	90.00
1.25	3939	2577	-5924	5840	832	614	90.00
1.50	3651	2289	-5924	5840	832	614	90.00
1.75	3424	2051	-5924	5840	832	614	90.00
2.00	3239	1877	-5924	5840	832	614	90.00
2.25	3084	1724	-5924	5840	832	614	90.00
2.50	2957	1675	-5924	5840	832	614	90.00
2.75	2847	1485	-5924	5840	832	614	90.00
3.00	2751	1329	-5924	5840	832	614	90.00
3.25	2688	1205	-5924	5840	832	614	90.00
3.50	2694	1231	-5924	5840	832	614	90.00
3.75	2538	1166	-5924	5840	832	614	90.00
4.00	2477	1107	-5924	5840	832	614	90.00
4.25	2416	1053	-5924	5840	832	614	90.00
4.50	2367	1005	-5924	5840	832	614	90.00
4.75	2321	951	-5924	5840	832	614	90.00
5.00	2283	921	-5924	5840	832	614	90.00
5.25	2247	884	-5924	5840	832	614	90.00
5.50	2213	850	-5924	5840	832	614	90.00
5.75	2181	819	-5924	5840	832	614	90.00
6.00	2152	790	-5924	5840	832	614	90.00



DETERMINATION OF CLOSING TIME

VALVE SIZE 12 VALVE CLASS 150

ACTUATOR 13-11, N721C-SR8D-M3HW

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Upward

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 7770

ACTUATOR VOLUME	,72	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>
MEDIA	<u>H2</u>		VALVE C <sub>v</sub>	<u>4942</u>
HYDRODYNAMIC TORQUE @ 90	<u>701</u>		SHUT OFF PRESSURE DROP	<u>45</u> PSI
PACKING TORQUE	<u>752</u>	IN.LBS.	SEAL TORQUE	<u>1143</u> IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.703</u> IN.
BUILDING PRESSURE	<u>45</u>	PSIG	dt	<u>0.1</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	,0741	69.4	44.9
20	,0750	138.9	44.7
30	,0774	260.5	43.9
40	,0836	395.2	41.8
50	,0952	510.4	37.2
60	,1120	558.7	27.9
70	,154	553.3	13.5
80	,164	575.6	8.39
90	,173	545.4	4.86



**DETERMINATION OF CLOSING TIME**

IN THE SEAT TRACT WITH A 2010 SEAL ACTUATOR

THE VALVE IS IN THE NON-PREFERRED DIRECTION

Tearing begin= 5930

ACT. VOL.= .70

SEAT RADIUS= .5

VALVE C. = 74.5

PACKING TORQUE= 756

BUILDING PRESSURE= 45

Tearing ending 3770

ACT. YOKE RADIUS= 1.5

VALVE C. = 74.5

SEAL TORQUE= 1183

ACT. PRESS= 30

ACTNG. TORQUE S. 0= 730

Dstem= 1.25

SOL. VALVE Cv= 2.06

ACTNG. TORQUE S. 0= 730

Dgage= 11.703

DEC.

10

20

30

40

50

60

70

80

90

DENSITY

.0741

.0750

.0771

.0838

.0952

.1100

.1140

.1140

.1170

VELOCITY

69.4

135.9

260.5

395.2

510.4

558.7

553.3

575.3

545.4

PRES DROP

44.90

44.70

43.90

41.80

37.20

27.90

13.50

9.39

4.86

TIME sec	TORQUE torque to open air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	4395	5913	-5924	3197	756	454	90.00
0.10	3737	5307	-5924	3197	756	454	90.00
0.20	3301	4818	-5924	3197	756	454	90.00
0.30	2898	4415	-5924	3197	756	454	90.00
0.40	2520	4077	-5924	3197	756	454	90.00
0.50	2271	3788	-5924	3197	756	454	90.00
0.60	2022	3539	-5924	3197	756	454	90.00
0.70	1805	3322	-5924	3197	756	454	90.00
0.80	1613	3130	-5924	3197	756	454	90.00
0.90	1443	2940	-5924	3197	756	454	90.00
1.00	1271	2803	-5924	3197	756	454	90.00
1.10	1154	2671	-5924	3197	756	454	90.00
1.20	1030	2548	-5924	3197	756	454	90.00
1.30	913	2438	-5924	3197	756	454	90.00
1.40	815	2332	-5924	3197	756	454	90.00
1.50	720	2238	-5924	3197	756	454	90.00
1.60	638	2151	-5924	3197	756	454	90.00
1.70	553	2070	-5924	3197	756	454	90.00
1.80	479	1996	-5924	3197	756	454	90.00
1.90	410	1927	-5924	3197	756	454	90.00
2.00	345	1862	-5924	3197	756	454	90.00
2.10	285	1802	-5924	3197	756	454	90.00
2.20	227	1743	-5924	3197	756	454	90.00
2.30	176	1693	-5924	3197	756	454	90.00
2.40	126	1643	-5924	3197	756	454	90.00
2.50	77	1593	-5924	3197	756	454	90.00
2.60	35	1552	-5924	3197	756	454	90.00
2.70	0	1510	-5924	3197	756	454	90.00
2.80	0	1471	-5924	3197	756	454	90.00
2.90	0	1431	-5924	3197	756	454	90.00
2.90	0	1401	-5924	3197	756	454	90.00
2.90	0	2570	-4858	1390	453	454	84.05
3.00	0	3381	-4154	-135	453	454	78.30
3.10	0	3337	-3377	-99	453	454	50.00
3.20	0	2229	-2871	-264	453	454	53.98
3.30	0	1692	-2731	-58	453	454	12.52
3.40	0	1787	-2675	-19	453	454	55.00
3.50	0	1839	-2742	-5	453	454	24.77
3.60	0	1989	-2896	-1	453	454	17.49
3.70	0	2240	-3115	0	453	454	11.11
3.80	0	2480	-3388	-0	453	454	5.55
3.90	0	1806	-3695	-0	1434	454	0.73



DETERMINATION OF CLOSING TIME

VALVE SIZE 12" VALVE CLASS 150

ACTUATOR B.C.L., N721C-SR80-4144

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Non-Recirc.

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 2770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>
MEDIA	<u>A1-</u>		VALVE C <sub>v</sub>	<u>4942</u>
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u> PSI
PACKING TORQUE	<u>756</u>	IN.LBS.	SEAL TORQUE	<u>1183</u> IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.723</u> IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	d <sub>c</sub>	<u>.25</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0740</u>	<u>69.5</u>	<u>44.9</u>
20	<u>.0744</u>	<u>130.8</u>	<u>44.8</u>
30	<u>.0760</u>	<u>205.9</u>	<u>44.1</u>
40	<u>.0797</u>	<u>409.9</u>	<u>42.4</u>
50	<u>.0877</u>	<u>549.0</u>	<u>38.5</u>
60	<u>.102</u>	<u>633.8</u>	<u>31.6</u>
70	<u>.128</u>	<u>653.9</u>	<u>18.5</u>
80	<u>.135</u>	<u>700.5</u>	<u>11.9</u>
90	<u>.152</u>	<u>624.9</u>	<u>5.95</u>



**DETERMINATION OF CLOSING TIME**

THE VALVE IS IN THE NON-PREFERRED DIRECTION

Testing begins 5930

ACT. VOL.= .72

MEDIUM= AIR

PACKING TORQUE= 756

BUILDING PRESSURE= 3.1

Testing ending 3770

ACT. YOKE RADIUS= 2.5

VALVE CV= 4942

SEAL TORQUE= 1183

ACT. PRESS= 80

HYDRO. TORQUE + YOKE= 756

Distem= 1.25

SOL. VALVE CV= 2.23

CHMR. CV= 1183. CHMR. = 45

Dage= 11.703

DEG.	10	20	30	40	50	60	70	80	90
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CHEMISTY	.0740	.0744	.0750	.0757	.0771	.0800	.0830	.0860	.0890
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VELOCITY	69.5	136.3	265.9	409.9	549.0	633.8	653.9	700.5	624.9
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PRES DROP	44.90	44.80	44.10	42.40	38.50	31.60	18.50	11.90	5.95
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TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA ° psi
0.00	11966	12993	-5924	3637	756	454	90.00	5.95
0.25	4844	5377	-5724	3637	756	454	90.00	5.95
0.50	3239	4276	-5924	3687	756	454	90.00	5.95
0.75	2456	3483	-5924	3687	756	454	90.00	5.95
1.00	1730	2958	-5724	3687	756	454	90.00	5.95
1.25	1550	2577	-5924	3687	756	454	90.00	5.95
1.50	1262	2289	-5924	3687	756	454	90.00	5.95
1.75	1038	2031	-5724	3687	756	454	90.00	5.95
2.00	850	1877	-5924	3687	756	454	90.00	5.95
2.25	698	1724	-5924	3687	756	454	90.00	5.95
2.50	588	1573	-5924	3687	756	454	90.00	5.95
2.75	458	1485	-5924	3687	756	454	90.00	5.95
3.00	362	1389	-5924	3687	756	454	90.00	5.95
3.25	277	1305	-5724	3687	756	454	90.00	5.95
3.50	205	1231	-5924	3687	756	454	90.00	5.95
3.75	139	1156	-5924	3687	756	454	90.00	5.95
4.00	80	107	-5724	3687	756	454	90.00	5.95
4.25	27	1053	-5924	3687	756	454	90.00	5.95
4.50	0	1005	-5924	3687	756	454	90.00	5.95
4.75	0	1384	-5174	1081	453	454	96.37	3.29
5.00	0	3497	-3942	-462	453	454	76.09	14.48
5.25	0	1915	-2751	-72	453	454	43.90	40.87
5.50	0	1707	-2012	-1	453	454	29.53	44.73
5.75	0	2490	-3398	-0	453	454	5.47	44.74



DETERMINATION OF CLOSING TIME

VALVE SIZE 12" VALVE CLASS 150

ACTUATOR Bell & Gossett N721C - SR80 - M3HW

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Per Fwd.

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u>	IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>	
MEDIA	<u>H2O</u>		VALVE C <sub>v</sub>	<u>4942</u>	
HYDRODYNAMIC TORQUE @ 90	<u>701</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>756</u>	IN.LBS.	SEAL TORQUE	<u>1183</u>	IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.703</u>	IN.
BUILDING PRESSURE	<u>45</u>	PSIG	dt	<u>.05</u>	SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0741</u>	<u>69.4</u>	<u>14.9</u>
20	<u>.0751</u>	<u>135.7</u>	<u>47.6</u>
30	<u>.0778</u>	<u>259.2</u>	<u>93.8</u>
40	<u>.0946</u>	<u>390.3</u>	<u>41.4</u>
50	<u>.0987</u>	<u>492.4</u>	<u>36.4</u>
60	<u>.135</u>	<u>494.9</u>	<u>22.7</u>
70	<u>.157</u>	<u>530.8</u>	<u>12.7</u>
80	<u>.166</u>	<u>556.7</u>	<u>7.82</u>
90	<u>.175</u>	<u>530.2</u>	<u>4.59</u>



DETERMINATION OF CLOSING TIME

DETERMINED WITH A DISPLACEMENT METER

THE VALVE IS IN THE PREFERRED DIRECTION

Spring Deadat 5420  
ACT. VOL. = .70  
MEDIA AIR  
PACKING TORQUE= 756  
BUILDING PRESSURE= 45

Spring Ending 3770  
ACT. VOL. 5400 US= 0.5

ACT. PRESS= 80  
Act. Vol. = 0.5  
Diam= 1.25

SOL. VALVE Ctr= 0.05  
Diam= 1.25  
Dgage= 11.703

DEG.	10	20	30	40	50	60	70	80	90
DENSITY	.0741	.0751	.0759	.0815	.0907	.1050	.1570	.1650	.1750
VELOCITY	69.4	135.7	259.2	390.3	497.4	494.9	533.9	556.7	530.2
PRES DROP	44.90	44.60	43.80	41.40	36.40	22.70	12.70	7.82	4.59

LOCA CLOSES THE VALVE TO 68 DEGREES WITH THE ACTUATOR STILL ACTUATED

MAXIMUM AERODYNAMIC TORQUE AS VALVE CLOSES IS 2700 IN-LBS. AT 30 DEGREES

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	0	4675	-3372	2100	155	454	58.04	14.70
0.05	0	2950	-2978	-880	453	454	58.32	24.99
0.10	0	2342	-2825	-425	453	454	51.16	34.81
0.15	0	2287	-2770	-22	453	454	45.17	32.61
0.20	0	1910	-2701	-117	453	454	39.85	41.43
0.25	0	1829	-2675	-61	453	454	35.02	42.59
0.30	0	1705	-2634	-29	453	454	30.33	43.55
0.35	0	1827	-2720	-15	453	454	26.45	44.08
0.40	0	1878	-2779	-7	453	454	22.59	44.39
0.45	0	2781	-3357	-6	453	454	17.47	44.59
0.50	0	2046	-2952	-1	453	454	15.59	44.73
0.55	0	2156	-3064	-0	453	454	12.44	44.82
0.60	0	2292	-3173	-0	453	454	7.50	44.70
0.65	0	2417	-3325	-0	453	454	6.78	44.93
0.70	0	2563	-3471	-0	453	454	4.25	44.75
0.75	0	2696	-3523	-0	453	454	1.71	44.43
0.80	0	1713	-3743	-0	1575	454	0.30	44.99



DETERMINATION OF CLOSING TIMEVALVE SIZE 12 VALVE CLASS 150ACTUATOR Bell, N721C-SR80-M3HWAMOUNT OF VALVE OPENING 90°DIRECTION OF FLOW No preference

## ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YOKE RADIUS	<u>2.5</u>	IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>	
MEDIA	<u>Air</u>		VALVE C <sub>v</sub>	<u>4942</u>	
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>751</u>	IN.LBS.	SEAL TORQUE	<u>1183</u>	IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.703</u>	IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.25</u>	SEC.

<u>DEG.</u>	<u>LOCA TORQUE (IN.LBS)</u>
10	<u>1234</u>
20	<u>1113</u>
30	<u>855</u>
40	<u>1473</u>
50	<u>2204</u>
60	<u>1940</u>
70	<u>1111</u>
80	<u>1743</u>
90	<u>5174</u>



DETERMINATION OF SEALING TORQUE

THE VALVE IS IN THE NON-PREFERRED DIRECTION

Spool length 5930	Spool ending 3770	ACT. PRESS= 90	SOL. VALVE C= 2.23
ACT. VOL.= .72	ACT. VALVE RADIUS= 2.5	HYDRO. TORQUE @ 70= 751	SHUT-OFF PRESS. CRIMP= 45
MEDIA=AIR	VALVE C/C= 4942	Offset= 1.08	Offset= 11.703
PACKING TORQUE= 756	SEAL TORQUE= 1133		
BUILDING PRESSURE= 3.1			

DEG.	10	20	30	40	50	60	70	80	90
LOAD TORQUE	1234	1113	886	1070	2207	2740	2222	1770	3274

TIME	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	ANGLE
sec	tend to open	air	spring	flow	packing & seal	bearing	degrees	
0.00	12240	12993	-5924	3963	756	454	90.00	
0.25	11720	3370	-5924	3963	756	454	90.00	
0.50	3525	4276	-5924	3963	756	454	90.00	
0.75	2732	3483	-5924	3963	756	454	90.00	
1.00	2235	2953	-5924	3963	756	454	90.00	
1.25	1824	2577	-5924	3963	756	454	90.00	
1.50	1538	2289	-5924	3963	756	454	90.00	
1.75	1311	2082	-5924	3963	756	454	90.00	
2.00	1126	1877	-5924	3963	756	454	90.00	
2.25	973	1724	-5924	3963	756	454	90.00	
2.50	844	1595	-5924	3963	756	454	90.00	
2.75	734	1485	-5924	3963	756	454	90.00	
3.00	638	1399	-5924	3963	756	454	90.00	
3.25	555	1305	-5924	3963	756	454	90.00	
3.50	481	1231	-5924	3963	756	454	90.00	
3.75	415	1166	-5924	3963	756	454	90.00	
4.00	366	1107	-5924	3963	756	454	90.00	
4.25	303	1053	-5924	3963	756	454	90.00	
4.50	254	1005	-5924	3963	756	454	90.00	
4.75	211	961	-5924	3963	756	454	90.00	
5.00	170	921	-5924	3963	756	454	90.00	
5.25	134	884	-5924	3963	756	454	90.00	
5.50	100	850	-5924	3963	756	454	90.00	
5.75	68	819	-5924	3963	756	454	90.00	
6.00	39	790	-5924	3963	756	454	90.00	



APPENDIX D

Determination of the Closing Times of  
Valves AOV104, 105, 107, 110 & 111 in  
the Preferred Direction.



DETERMINATION OF CLOSING TIME

VALVE SIZE 14" VALVE CLASS 150

ACTUATOR Bell &amp; Gossett N721C-SR30-M3HW

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Perfume

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>40</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>
MEDIA	<u>H2O</u>		VALVE C <sub>v</sub>	<u>0.317</u>
HYDRODYNAMIC TORQUE @ 90	<u>1182</u>		SHUT OFF PRESSURE DROP?	<u>4.5</u> PSI
PACKING TORQUE	<u>832</u>	IN.LBS.	SEAL TORQUE	<u>1454</u> IN.LBS.
STEM DIA.	<u>1.375</u>	IN.	GAGE DIA.	<u>12.974</u> IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.05</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0739</u>	<u>65.3</u>	<u>44.9</u>
20	<u>.0743</u>	<u>128.7</u>	<u>44.8</u>
30	<u>.0757</u>	<u>250.7</u>	<u>44.2</u>
40	<u>.0790</u>	<u>388.7</u>	<u>42.6</u>
50	<u>.0861</u>	<u>529.0</u>	<u>39.3</u>
60	<u>.0983</u>	<u>661.7</u>	<u>33.1</u>
70	<u>.124</u>	<u>845.5</u>	<u>20.7</u>
80	<u>.142</u>	<u>1033.0</u>	<u>11.1</u>
90	<u>.149</u>	<u>128.1</u>	<u>6.92</u>

III

III

III

**DETERMINATION OF CLIPPING TIME**

THE VALUE IS IN THE PREFERRED DIRECTION

Tracing engine 5730  
ACT. VOL. 1.70  
VECTERATEIN  
PACKING TORQUE= 832  
BUILDING PRESSURE= 3.1

Tipping engine 5770  
ACT. VOL. 1.70  
VECTERATEIN  
SEAL TORQUE= 1454

ACT. PRESS= 30  
HYDRO. TORQUE= 1454  
Diam= 1.375

TRUE VALUE OF 0.25  
SHUT OFF POSITION= 45  
Ogage= 12.974

DEG.	10	20	30	40	50	60	70	80	90
DEMSIT	.0737	.0743	.0757	.0790	.0851	.0930	.1010	.1120	.1230
VELOCITY	35.3	129.7	250.7	388.4	529.0	621.7	645.5	633.4	628.1
PRES DROP	44.90	44.80	44.20	42.60	39.30	33.10	20.70	11.10	6.92

TIME sec	FORNUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	2083	12993	-5924	-6431	832	614	90.00	6.92
0.05	0	11823	-5724	-6431	832	614	90.30	6.92
0.10	0	10375	-5924	-6431	832	614	90.00	6.92
0.15	0	10783	-4492	-7404	499	614	81.32	10.54
0.20	0	6662	-3204	-3931	499	614	56.30	25.23
0.25	0	2730	-2858	-985	499	614	53.21	37.30
0.30	0	2091	-2775	-429	499	614	46.29	40.62
0.35	0	1320	-2775	-120	499	614	40.73	42.29
0.40	0	1685	-2679	-120	499	614	36.31	43.13
0.45	0	1626	-2678	-62	499	614	32.16	43.35
0.50	0	1317	-2700	-32	499	614	29.54	44.22
0.55	0	1647	-2742	-19	499	614	24.77	44.51
0.60	0	1697	-2801	-9	499	614	21.41	44.71
0.65	0	2737	-2873	-5	499	614	18.14	44.91
0.70	0	1853	-2964	-2	499	614	15.24	44.94
0.75	0	1953	-3065	-1	499	614	12.41	44.87
0.80	0	2084	-3177	-0	499	614	9.72	44.73
0.85	0	2187	-3300	-0	499	614	7.24	44.92
0.90	0	2319	-3432	-0	499	614	4.29	44.25
0.95	0	2773	-3672	-0	731	614	2.39	44.17
1.00	0	1394	-3690	-0	1681	614	1.01	44.78



DETERMINATION OF CLOSING TIMEVALVE SIZE 14" VALVE CLASS 150ACTUATOR B-11, N721C-SR80-M3HWAMOUNT OF VALVE OPENING 90°DIRECTION OF FLOW Preferred

## ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770ACTUATOR VOLUME .7L SCFACTUATOR YOKE RADIUS 2.5 IN.ACTUATOR PRESSURE 80 PSIGSOLENOID VALVE C<sub>v</sub> 2.26MEDIA AIRVALVE C<sub>v</sub> 6317HYDRODYNAMIC TORQUE @ 90 118LSHUT OFF PRESSURE DROP 45 PSIPACKING TORQUE 832 IN.LBS.SEAL TORQUE 1454 IN.LBS.STEM DIA. 1.375 IN.GAGE DIA. 12.974 IN.BUILDING PRESSURE 3.1 PSIGdt .05 SEC.DEG.      LOCA TORQUE (IN.LBS)10 14320 130330 88840 750 -149260 -311370 -749680 -958490 -7586



## DETERMINATION OF DELAY TIME

THE VALVE IS IN THE PREFERRED DIRECTION

TRIPPING RADIUS 5030      TRIPPING RADIUS 3770  
 ACT. VOL. + .72      ACT. VOL. RADIUS 1.6

ACT. PRESSURE 40

SOL. VALVE Inv 2.25

MEDIAN TIME

VALVE INV 2.25

STICK SLIP TIME 1.132

CHUCK UP TIME 4.8

PACKING TORQUE = 832

SEAL TORQUE = 1454

DSTEM = 1.375

Dgage = 12.974

BUILDING PRESSURE = 3.1

DEG.      10      20      30      40      50      60      70      80      90

LOCK TORQUE      1413      1303      993      7      1972      3113      7495      9824      7693

LOCA CLOSES THE VALVE TO 69 DEGREES WITH THE ACTUATOR STILL ACTUATED

MAXIMUM AERODYNAMIC TORQUE AS VALVE CLOSES IS -9917 IN.LBS. @ 80 DEGREES

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees
0.03	0	1000	-3353	993	499	614	33.00
0.05	0	3953	-2772	-2294	499	614	45.70
0.10	0	2620	-2577	-1057	499	614	35.66
0.15	0	2100	-2592	-527	499	614	29.33
0.20	0	1966	-2745	-334	499	614	24.30
0.25	0	1874	-2818	-169	499	614	20.62
0.30	0	1903	-2924	112	499	614	17.00
0.35	0	1967	-3002	-79	499	614	14.10
0.40	0	2046	-3113	-47	499	614	11.23
0.45	0	2353	-3253	-234	499	614	8.88
0.50	0	2975	-3374	-614	499	614	5.38
0.55	0	3453	-3549	-1017	499	614	3.03
0.60	0	2540	-3755	-1420	499	614	0.44



DETERMINATION OF CLOSING TIME

VALVE SIZE 12 VALVE CLASS 150

ACTUATOR Bell's N721C-SR80-M314W

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW Preface

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.25</u>
MEDIA	<u>Air</u>		VALVE C <sub>v</sub>	<u>.9942</u>
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u> PSI
PACKING TORQUE	<u>756</u>	IN.LBS.	SEAL TORQUE	<u>1183</u> IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.703</u> IN.
BUILDING PRESSURE	<u>45</u>	PSIG	dt	<u>.65</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0741</u>	<u>69.4</u>	<u>44.9</u>
20	<u>.0750</u>	<u>135.9</u>	<u>44.7</u>
30	<u>.0774</u>	<u>260.5</u>	<u>43.9</u>
40	<u>.0836</u>	<u>395.2</u>	<u>41.8</u>
50	<u>.0902</u>	<u>510.4</u>	<u>37.2</u>
60	<u>.120</u>	<u>558.7</u>	<u>27.9</u>
70	<u>.154</u>	<u>553.3</u>	<u>13.5</u>
80	<u>.164</u>	<u>575.6</u>	<u>8.39</u>
90	<u>.173</u>	<u>545.7</u>	<u>4.86</u>



DETERMINATION OF CLOSING TIME

THE VALVE IS IN THE PREFERRED DIRECTION

Spring begin <sup>n</sup> 5430	Spring ending 3770	ACT. VOL.= .72	ACT. VOKE RADIUS= 2.5	ACT. PRESS= 80	SOL. VALVE CV= 2.25
VALVE DIA= 3.42	VALVE DIA= 3.42	VALVE DIA= 3.42	VALVE DIA= 3.42	VALVE DIA= 3.42	SHUT OFF REB. GRAD= 5
PACKING TORQUE= 755	SEAL TORQUE= 1183	DIA= 1.25	DIA= 1.25	DIA= 1.25	Diaage= 11.703
BUILDING PRESSURE= 45					

DEG.	10	20	30	40	50	60	70	80	90
DEENSITY	.0741	.0750	.0774	.0836	.0952	.1203	.1546	.1846	.1750
VELOCITY	59.4	135.9	260.5	395.2	510.4	558.7	553.3	575.6	545.4
PRES DROP	44.90	44.70	43.90	41.80	37.20	27.90	13.50	9.39	4.86

LOCA CLOSES THE VALVE TO 47 DEGREES WITH THE ACTUATOR STILL ACTUATED

MAXIMUM AERODYNAMIC TORQUE AS VALVE CLOSES IS 3177 IN-LBS. AT 90 DEGREES

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	0	4661	-3319	-2156	453	454	57.03	47.81
0.05	0	2909	-2945	-872	453	454	57.12	30.67
0.10	0	2273	-2909	-372	453	454	49.76	37.21
0.15	0	-547	-2734	-202	453	454	44.13	39.12
0.20	0	1391	-2693	-106	453	454	38.90	42.03
0.25	0	1821	-2675	-54	453	454	34.15	43.02
0.30	0	1803	-2697	-25	453	454	29.77	43.21
0.35	0	1835	-2729	-13	453	454	25.70	44.24
0.40	0	1890	-2792	-6	453	454	21.83	44.54
0.45	0	1737	-2674	-3	453	454	18.51	44.75
0.50	0	2066	-2972	-1	453	454	14.98	44.30
0.55	0	2179	-3086	-0	453	454	11.36	44.85
0.60	0	2303	-3214	-0	453	454	8.77	44.51
0.65	0	2444	-3352	-0	453	454	6.28	44.93
0.70	0	2592	-3500	-0	453	454	3.77	44.96
0.75	0	2707	-3555	-0	1273	454	1.18	44.79



DETERMINATION OF CLOSING TIME

VALVE SIZE 12" VALVE CLASS 150

ACTUATOR B.FLIS N721C-SR80-H2HW

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW P.L.C.

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 2770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>
MEDIA	<u>H2</u>		VALVE C <sub>v</sub>	<u>4942</u>
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u> PSI
PACKING TORQUE	<u>757</u>	IN.LBS.	SEAL TORQUE	<u>1183</u> IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.703</u> IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.05</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>.0740</u>	<u>69.5</u>	<u>44.9</u>
20	<u>.0744</u>	<u>136.8</u>	<u>44.8</u>
30	<u>.0760</u>	<u>205.9</u>	<u>44.1</u>
40	<u>.0797</u>	<u>209.9</u>	<u>42.4</u>
50	<u>.0877</u>	<u>149.0</u>	<u>38.5</u>
60	<u>.102</u>	<u>633.8</u>	<u>31.6</u>
70	<u>.128</u>	<u>653.9</u>	<u>18.5</u>
80	<u>.135</u>	<u>700.5</u>	<u>11.9</u>
90	<u>.152</u>	<u>624.9</u>	<u>5.95</u>



**DETERMINATION OF CLOSING TIME**

THE VALVE IS IN THE PREFERRED DIRECTION

Spring Design 5930 Spring rating 3770  
 ACT. VOL. = .70 ACT. YOLK RADIUS = 2.5  
 DESIGN VOL. = .742 VALVE ST. = 4.2  
 PACKING TORQUE = 756 SEAL TORQUE = 1193  
 BUILDING PRESSURE = 3.1

ACT. PRESS = 30  
 ACTUAL TORQUE = 756  
 Diam = 1.25

SOL. VALVE Cv = 0.26  
 SHUT OFF PRES. DRAG =  
 Dgage = 11.703

DEC.	10	20	30	40	50	60	70	80	90
DENSITY	.740	.744	.748	.752	.757	.762	.768	.775	.782
VELOCITY	69.5	136.8	265.9	409.9	549.0	683.8	813.9	940.5	1049.9
PRES DROP	44.90	44.80	44.10	42.40	38.50	31.60	18.50	11.90	5.95

TIME sec	TORQUE tend to open	TORQUE at	TORQUE spring	TORQUE film	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	4591	12993	-5924	-3687	756	454	90.00	5.95
0.05	5127	13328	-5924	-3597	756	454	90.00	5.95
0.10	1974	10375	-5924	-3497	756	454	90.00	5.95
0.15	1040	9442	-5924	-3397	756	454	90.00	5.95
0.20	255	5468	-5924	-3297	756	454	90.00	5.95
0.25	0	8016	-5924	-3197	756	454	90.00	5.95
0.30	0	8392	-4779	-4521	453	454	83.50	9.81
0.35	0	3481	-3742	-3570	453	454	73.74	13.17
0.40	0	3671	-3035	-1494	453	454	61.62	29.47
0.45	0	2546	-2856	-598	453	454	53.06	35.38
0.50	0	2147	-2772	-273	453	454	46.52	39.32
0.55	0	1949	-2713	-144	453	454	41.09	41.97
0.60	0	1345	-2678	-75	453	454	36.14	43.05
0.65	0	2003	-2629	-33	453	454	31.11	45.35
0.70	0	1819	-2709	-18	453	454	27.41	44.28
0.75	0	1864	-2763	-9	453	454	23.48	44.35
0.80	0	1732	-2933	-4	453	454	19.31	44.35
0.85	0	2022	-2923	-2	453	454	16.38	44.33
0.90	0	2129	-3036	-1	453	454	13.17	44.86
0.95	0	2150	-3163	-1	453	454	10.10	44.89
1.00	0	2384	-3292	-0	453	454	7.40	44.92
1.05	0	2528	-3436	-0	453	454	4.83	44.95
1.10	0	2174	-3693	-0	453	454	2.3	44.97
1.15	0	1752	-3717	-0	1500	454	0.65	44.99



DETERMINATION OF CLOSING TIMEVALVE SIZE 12" VALVE CLASS 150ACTUATOR Bell & Gossett N721C-SR80-m3H4AMOUNT OF VALVE OPENING 90°DIRECTION OF FLOW Preferred

## ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 2770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YOKE RADIUS	<u>2.5</u>	IN.
ACTUATOR PRESSURE	<u>40</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>	
MEDIA	<u>Air</u>		VALVE C <sub>v</sub>	<u>4942</u>	
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>756</u>	IN.LBS.	SEAL TORQUE	<u>1183</u>	IN.LBS.
STEM DIA.	<u>.125</u>	IN.	GAGE DIA.	<u>.11703</u>	IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.05</u>	SEC.

DEG.	LOCA TORQUE (IN.LBS)
10	<u>1190</u>
20	<u>1093</u>
30	<u>756</u>
40	<u>61</u>
50	<u>-1061</u>
60	<u>-2011</u>
70	<u>-4729</u>
80	<u>-6776</u>
90	<u>-4404</u>



## DETERMINATION OF DELAY TIME

12 - 100 GROSS VALVE TESTER WITH AUTOMATIC ACTUATOR

THE VALVE IS IN THE PREFERRED DIRECTION

Tipping engine 5930	Tipping ending 3770	ACT. TORQUE = 90	SOL. VALVE DYN 2.35
ACT. VOLV. .73	ACT. TORQUE RADIUS = 1.5	ACT. PRESS = 90	SHUTTER PRES. DROP = 45
MEDIUM	VALVE C = 4742	MEDIUM TORQUE = 70 x 3.	
PACKING TORQUE = 756	SEAL TORQUE = 1183	Dynam. = 1.35	Ocage = 11.703
BUILDING PRESSURE = 3.1			

DEC.	10	20	30	40	50	60	70	80	90
LOCK TORQUE	1130	1073	763	31	-1061	-2311	-4729	-5776	-9404

TIME SEC	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees
0.00	2664	12993	-5924	-5614	756	454	90.00
0.05	1296	11823	-5924	-5614	756	454	70.00
0.10	47	10375	-5924	-5614	756	454	90.00
0.15	0	9442	-5924	-5614	756	454	90.00
0.20	0	11137	-4803	-7454	453	454	22.00
0.25	0	7776	-3331	-5353	453	454	57.53
0.30	0	4234	-2914	-2327	453	454	50.36
0.35	0	2905	-2678	-1115	453	454	37.51
0.40	0	2380	-2677	-610	453	454	32.24
0.45	0	2152	-2717	-343	453	454	26.70
0.50	0	2050	-2787	-102	453	454	22.00
0.55	0	2070	-2376	-102	453	454	18.22
0.60	0	2144	-2931	-71	453	454	14.73
0.65	0	2283	-3150	-43	453	454	11.53
0.70	0	2517	-3231	-194	453	454	8.61
0.75	0	3009	-3383	-533	453	454	5.73
0.80	0	3217	-3725	-932	776	454	2.77
0.85	0	2386	-3758	-1198	1616	454	0.10



DETERMINATION OF CLOSING TIMEVALVE SIZE 12"VALVE CLASS 150ACTUATOR Bell & Gossett N721C-SR80-M3HWAMOUNT OF VALVE OPENING 70°DIRECTION OF FLOW Preferred

## ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 7770ACTUATOR VOLUME .72 SCFACTUATOR YOKE RADIUS 2.5 IN.ACTUATOR PRESSURE 40 PSIGSOLENOID VALVE C<sub>v</sub> 2.26MEDIA AirVALVE C<sub>v</sub> 4942HYDRODYNAMIC TORQUE @ 90 761SHUT OFF PRESSURE DROP 45 PSIPACKING TORQUE 756 IN.LBS.SEAL TORQUE 1183 IN.LBS.STEM DIA. 1.75 IN.GAGE DIA. 11.703 IN.BUILDING PRESSURE 3.1 PSIGdt .05 SEC.DEG. LOCA TORQUE (IN.LBS)10 118020 109330 75640 6150 -106160 -201170 -472980 -677690 -4404



**DETERMINATION OF CLOSING TIME**

THE VALVE OPENING IS RESTRICTED TO 70 DEGS.

THE VALVE IS IN THE PREFERRED DIRECTION

Operating pressure = 90 psig

ACT. VOL. = .72

MEDIA=AIR

PACKING TORQUE = 1190

BUILDING PRESSURE = 3.1

Operating diameter = 177

ACT. YUKE RADIUS = 2.5

VALVE Cv = 4942

SCFM TORQUE = 1193

ACT. PRESS = 90

HYDRO. TORQUE @ 90 = 751

SCFM = 1193

SOL. VALVE Cv = 3.25

SHUT-OFF PRES. Cv = 45

SCFM = 1193

DEG.	10	20	30	40	50	60	70	80	90	100
LOCA TORQUE	1190	1093	756	61	-1061	-2611	-4729	-6775	-4404	

TIME	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	ANGLE
0.00	tend to open	417	SPRING	1190	packing x seat	SPRING	SPRING	0 deg
0.05	257	8475	-3488	-5939	756	454	70.00	
0.10	0	7520	-3488	-5939	756	454	70.00	
0.15	0	4442	-2889	-3010	453	454	34.73	
0.20	0	3209	-2726	-1391	453	454	42.15	
0.25	0	2502	-2675	-735	453	454	34.04	
0.30	0	2097	-2765	-229	453	454	23.32	
0.35	0	2053	-2950	-110	453	454	19.24	
0.40	0	2209	-2750	-70	453	454	15.35	
0.45	0	2338	-3066	-51	453	454	12.39	
0.50	0	2209	-3194	-102	453	454	9.39	
0.55	0	2209	-3397	-438	453	454	5.93	
0.60	0	3398	-3511	-784	453	454	3.91	
0.65	0	2996	-3716	-1132	1497	454	0.65	



APPENDIX E

Determination of the Closing Time of  
Valves AOV104, 105, 107, 110 & 111 in  
the Nonpreferred Direction with the  
Valve Opening Restricted to 70 Degrees



DETERMINATION OF CLOSING TIME

VALVE SIZE 14" VALVE CLASS 150

ACTUATOR Bettis N721C-SR90-M3HW

AMOUNT OF VALVE OPENING 70°

DIRECTION OF FLOW Non-pv. Closed

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u>	IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.74</u>	
MEDIA	<u>Air</u>		VALVE C <sub>v</sub>	<u>6317</u>	
HYDRODYNAMIC TORQUE @ 90	<u>1182</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>832</u>	IN.LBS.	SEAL TORQUE	<u>1454</u>	IN.LBS.
STEM DIA.	<u>1.375</u>	IN.	GAGE DIA.	<u>12.974</u>	IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.05</u>	SEC.

<u>DEG.</u>	<u>DENSITY (LBS/FT.<sup>3</sup>)</u>	<u>VELOCITY (FT/SEC)</u>	<u>PRESSURE DROP (PSI)</u>
10	<u>.0739</u>	<u>65.3</u>	<u>44.9</u>
20	<u>.0743</u>	<u>128.7</u>	<u>44.8</u>
30	<u>.0759</u>	<u>250.7</u>	<u>44.2</u>
40	<u>.0790</u>	<u>388.4</u>	<u>42.6</u>
50	<u>.0861</u>	<u>529.0</u>	<u>39.3</u>
60	<u>.0982</u>	<u>621.7</u>	<u>33.1</u>
70	<u>.124</u>	<u>643.5</u>	<u>20.7</u>
80	<u>.146</u>	<u>633.6</u>	<u>11.1</u>
90	<u>.149</u>	<u>628.1</u>	<u>6.92</u>



DETERMINATION OF CLOSING TIME

2000 GPM VALVE WITH HYDRAULIC ACTUATOR

THE VALVE OPENING IS RESTRICTED TO 70 DEGS.

THE VALVE IS IN THE NON-PREFERRED DIRECTION

FLOWING ENGINE= 3730	FEEDING ENGINE= 3770	ACT. VOL.= .72	ACT. YOLKE RADIUS= 2.5	ACT. PRESS= 80	SOL. VALVE Cv= 2.23
MEDIA=AIR	VALVE Cv= 6317			HYDRO. TORQUE @ 90= 1132	SHUT-OFF PRES. DROP= 45
WHEEL TORQUE= 100	SEAL TORQUE= 1764			Steam= 1.375	Drop= 12.71
BUILDING PRESSURE= 3.1					

DEG.	10	20	30	40	50	60	70	80	90	100
DENSITY	.0739	.0743	.0757	.0790	.0861	.0982	.1240	.1420	.1490	
VELOCITY	45.3	49.7	50.7	50.4	52.0	52.7	55.5	58.6	59.1	
PRES DROP	44.90	44.80	44.20	42.30	39.30	33.10	20.70	11.10	6.92	

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	4510	8475	-3488	-1922	932	614	70.00	20.70
0.05	3555	7520	-3488	-1922	932	614	70.00	20.70
0.10	2983	6767	-3488	-1922	932	614	70.00	20.70
0.15	2194	6158	-3488	-1922	932	614	70.00	20.70
0.20	1689	5654	-3488	-1922	932	614	70.00	20.70
0.25	1234	5229	-3488	-1922	932	614	70.00	20.70
0.30	900	4865	-3488	-1922	932	614	70.00	20.70
0.35	586	4550	-3488	-1922	932	614	70.00	20.70
0.40	310	4275	-3488	-1922	932	614	70.00	20.70
0.45	67	4032	-3488	-1922	932	614	70.00	20.70
0.50	0	3815	-3488	-1922	932	614	70.00	20.70
0.55	0	3777	-3121	-1137	499	614	35.39	20.70
0.60	0	2346	-2901	-557	499	614	55.33	35.99
0.65	0	1914	-2903	-224	499	614	49.47	37.47
0.70	0	1773	-2781	-123	499	614	44.33	41.67
0.75	0	1654	-2702	-65	499	614	40.03	42.68
0.80	0	1606	-2677	-42	499	614	35.84	43.26
0.85	0	1572	-2573	-23	499	614	31.73	43.39
0.90	0	1504	-2502	-15	499	614	23.16	44.30
0.95	0	1439	-2744	-8	499	614	24.55	44.52
1.00	0	1393	-2693	-3	499	614	21.31	44.71
1.05	0	1366	-2878	-2	499	614	18.16	44.91
1.10	0	1353	-2966	-1	499	614	15.17	44.94
1.15	0	1354	-3037	-2	499	614	12.35	44.95
1.20	0	2056	-3130	-0	499	614	9.69	44.90
1.25	0	2189	-3303	-0	499	614	7.19	44.91
1.30	0	2321	-3433	-0	499	614	4.34	44.75
1.35	0	1966	-3575	-0	994	614	2.65	44.97
1.40	0	1390	-3691	-0	1686	614	1.00	44.98



DETERMINATION OF CLOSING TIME

VALVE SIZE 14" VALVE CLASS 150

ACTUATOR Bettis N721C-SR80-M3HW

AMOUNT OF VALVE OPENING 70°

DIRECTION OF FLOW No preferred

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.7L</u>	SCF	ACTUATOR YOKE RADIUS	<u>2.5</u>	IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>	
MEDIA	<u>Air</u>		VALVE C <sub>v</sub>	<u>6317</u>	
HYDRODYNAMIC TORQUE @ 90	<u>1182</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>832</u>	IN.LBS.	SEAL TORQUE	<u>1454</u>	IN.LBS.
STEM DIA.	<u>.375</u>	IN.	GAGE DIA.	<u>12.924</u>	IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.05</u>	SEC.

DEG.	LOCA TORQUE (IN.LBS)
10	<u>1413</u>
20	<u>1315</u>
30	<u>170</u>
40	<u>363</u>
50	<u>-522</u>
60	<u>-1693</u>
70	<u>-1106</u>
80	<u>50</u>
90	<u>7287</u>



DETERMINATION OF CLOSING TIME

THE VALVE OPENING IS RESTRICTED TO 70 DEGS.

THE VALVE IS IN THE PREFERRED DIRECTION

Spring setting = 5430      Setting position = 1270  
 ACT. VOL. = .72      ACT. YOKE RADIUS = 2.5      SOL. VALVE Cv = 2.25  
 MEDIA=AIR      VALVE Cv = 6317      SHUT-OFF PRES. DACP = 45  
 PACKING TORQUE = 330      VALVE TORQUE = 1454      System = 1.375  
 BUILDING PRESSURE = 3.1      S, S, T = 12.374

DEG.	10	20	30	40	50	60	70	80	90	100
LOCA TORQUE	1477	1565	1858	2333	2786	2367	1106	2170	7297	

TIME	TORQUE	ANGLE						
0.00	6092	8475	-3488	-340	832	614	70.00	0.00 deg
0.10	4181	6564	-3488	-340	832	614	70.00	
0.20	3035	5413	-3488	-340	832	614	70.00	
0.30	2254	4637	-3488	-340	832	614	70.00	
0.40	1682	4065	-3488	-340	832	614	70.00	
0.50	1242	3515	-3488	-340	832	614	70.00	
0.60	893	3276	-3488	-340	832	614	70.00	
0.70	607	2990	-3488	-340	832	614	70.00	
0.80	397	2762	-3488	-340	832	614	70.00	
0.90	168	2551	-3488	-340	832	614	70.00	
1.00	0	2378	-3468	-340	832	614	70.00	
1.10	0	1092	3051	327	499	614	50.38	
1.20	0	683	-2906	1108	499	614	55.51	
1.30	0	475	-2840	1250	499	614	52.12	
1.40	0	338	-2902	1323	499	614	49.77	
1.50	0	431	-2787	1241	499	614	47.83	
1.60	0	517	-2772	1141	499	614	45.62	
1.70	0	501	-2737	1021	499	614	43.72	
1.80	0	706	-2701	881	499	614	39.89	
1.90	0	853	-2679	711	499	614	36.31	
2.00	0	1052	-2656	611	499	614	33.16	
2.10	0	1268	-2711	329	499	614	27.19	
2.20	0	1508	-2793	171	499	614	21.80	
2.30	0	1734	-2933	85	499	614	15.21	
2.40	0	1976	-3128	38	499	614	10.87	
2.50	0	2919	-3369	-563	499	614	5.99	
2.60	0	2663	-3722	1360	1004	614	0.00	



DETERMINATION OF CLOSING TIME

VALVE SIZE 12 VALVE CLASS 150

ACTUATOR Bettis N721C-SR80-M3HW

AMOUNT OF VALVE OPENING 70°

DIRECTION OF FLOW Non-reversed

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YORE RADIUS	<u>2.5</u> IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>
MEDIA	<u>AIR</u>		VALVE C <sub>v</sub>	<u>4942</u>
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u> PSI
PACKING TORQUE	<u>756</u>	IN.LBS.	SEAL TORQUE	<u>1183</u> IN.LBS.
STEM DIA.	<u>.125</u>	IN.	GAGE DIA.	<u>.11783</u> IN.
BUILDING PRESSURE	<u>45</u>	PSIG	dt	<u>.05</u> SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<u>10741</u>	<u>69.4</u>	<u>44.9</u>
20	<u>.0770</u>	<u>135.9</u>	<u>44.7</u>
30	<u>.0724</u>	<u>260.5</u>	<u>43.9</u>
40	<u>.0836</u>	<u>395.2</u>	<u>41.8</u>
50	<u>.0902</u>	<u>510.4</u>	<u>37.2</u>
60	<u>.120</u>	<u>558.7</u>	<u>27.9</u>
70	<u>.154</u>	<u>553.3</u>	<u>13.5</u>
80	<u>.164</u>	<u>575.6</u>	<u>8.39</u>
90	<u>.173</u>	<u>545.4</u>	<u>4.86</u>



**DETERMINATION OF CLOSING TIME**

FOR A 10 IN. DIA. VALVE WITH A 1000 LB. SHUT-OFF WEIGHT

THE VALVE OPENING IS RESTRICTED TO 70 DEGS.

THE VALVE IS IN THE NON-PREFERRED DIRECTION

SPRING DEPTH = 3730	TESTING ANGLES 0-70	ACT. VOL. = .72	ACT. YOKE RADIUS = 2.6	ACT. PRESS = 90	SOL. VALVE Cv = 2.25
MEDIA=AIR	VALVE Cv = 4942			HYDRO. TORQUE @ 90 = 761	SHUT-OFF PCS. ORCP = 45
PACKING TORQUE = 783	SEAL TORQUE = 1.33			SYSTEM = 1.25	System Cv = 11.703
BUILDING PRESSURE = 45					

DEG.	0	20	30	40	50	60	70	80	90	70
DENSITY	.0741	.0750	.0774	.0836	.0962	.1200	.1540	.1640	.1730	
VELOCITY	39.4	105.7	250.5	375.2	510.4	630.7	683.2	698.3	712.4	
PRES DROP	44.90	44.70	43.40	41.80	37.20	27.70	13.50	9.39	4.86	

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	583	3857	-3488	-995	756	454	70.00	13.50
0.05	389	3659	-3488	-995	756	454	70.00	13.50
0.10	207	3481	-3488	-995	756	454	70.00	13.50
0.15	45	3320	-3488	-995	756	454	70.00	13.50
0.30	0	3173	-3488	-995	756	454	70.00	13.50
0.35	0	2785	-2774	-377	453	454	33.42	22.42
0.30	0	2444	-2949	-403	453	454	57.09	30.41
0.35	0	2097	-2827	-179	453	454	51.30	35.98
0.40	0	1755	-2773	-87	453	454	45.74	37.03
0.45	0	1850	-2711	-46	453	454	40.93	41.36
0.50	0	1798	-3478	-27	453	454	34.24	42.58
0.55	0	2787	-2777	-13	453	454	31.31	33.51
0.60	0	1808	-2707	-9	453	454	27.65	44.03
0.65	0	1855	-2758	-4	453	454	23.73	44.40
0.70	0	1924	-2931	-	453	454	20.05	44.87
0.75	0	2014	-2921	-0	453	454	16.60	44.76
0.80	0	2120	-3028	-0	453	454	13.33	44.23
0.85	0	2201	-3179	-0	453	454	10.03	44.34
0.90	0	2374	-3282	-0	453	454	7.57	44.92
0.95	0	2517	-3425	-0	453	454	5.00	44.94
1.00	0	2691	-3577	-0	453	454	2.02	44.37
1.05	0	1775	-3710	-0	1480	454	0.73	44.99



DETERMINATION OF CLOSING TIME

VALVE SIZE 11" VALVE CLASS 150

ACTUATOR Bell & Gossett 1721C-SR 80-M3HW

AMOUNT OF VALVE OPENING 70°

DIRECTION OF FLOW No preference

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 7770

ACTUATOR VOLUME ,72 SCF ACTUATOR YORE RADIUS 2.5 IN.  
ACTUATOR PRESSURE 80 PSIG SOLENOID VALVE C<sub>v</sub> 2.26  
MEDIA Air VALVE C<sub>v</sub> .4942  
HYDRODYNAMIC TORQUE @ 90 761 SHUT OFF PRESSURE DROP .45 PSI  
PACKING TORQUE 736 IN.LBS. SEAL TORQUE 1163 IN.LBS.  
STEM DIA. 1.25 IN. GAGE DIA. 11.703 IN.  
BUILDING PRESSURE 3.1 PSIG dt .05 SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	.0740	69.5	44.9
20	.0744	130.8	44.8
30	.0760	205.9	44.1
40	.0797	409.9	42.4
50	.0877	549.0	38.5
60	.102	633.8	31.6
70	.128	653.9	18.5
80	.135	700.5	11.9
90	.152	627.9	5.95



**DETERMINATION OF CLOSING TIME**

THE VALVE OPENING IS RESTRICTED TO 70 DEGS.

THE VALVE IS IN THE NON-PREFERRED DIRECTION

Spring begin= 6930	Spring ending 3773	ACT. VOL.= .72	ACT. YOKE RADIUS= 2.5	ACT. PRESS= 80	SCL. VALVE CV= 2.26
MEDIA=AIR	VALVE CV= 4942	HYDRO. TORQUE @ 90= 761	SHUT-OFF PRES. DROP= 45		
OPENING TORQUE= 761	SEAL TORQUE= 1.03	Open= 1.25	Drop= 11.743		
BUILDING PRESSURE= 3.1					

DEG.	10	20	30	40	50	60	70	80	90
DENSITY	.0740	.0744	.0760	.0797	.0877	.1020	.1280	.1350	.1520
VELOCITY	39.3	133.3	233.7	407.7	547.0	833.3	833.7	700.0	524.3
PRES DROP	44.90	44.80	44.10	42.40	33.50	31.60	18.50	11.70	5.73

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	5040	9475	-3488	-1156	756	454	70.00	18.50
0.05	4085	7520	-3488	-1156	756	454	70.00	18.50
0.10	3383	5777	-3488	-1156	756	454	70.00	18.50
0.15	2724	6158	-3488	-1156	756	454	70.00	18.50
0.20	2219	5654	-3488	-1156	756	454	70.00	18.50
0.25	1794	5929	-3488	-1156	756	454	70.00	18.50
0.30	1431	4865	-3488	-1156	756	454	70.00	18.50
0.35	1113	4550	-3488	-1156	756	454	70.00	18.50
0.40	847	4275	-3488	-1156	756	454	70.00	18.50
0.45	597	4032	-3488	-1156	756	454	70.00	18.50
0.50	381	3815	-3488	-1156	756	454	70.00	18.50
0.55	132	3512	-3488	-1156	756	454	70.00	18.50
0.60	13	3447	-3488	-1156	756	454	70.00	18.50
0.65	0	3299	-3488	-1156	756	454	70.00	18.50
0.70	0	3025	-3134	-787	453	454	37.50	23.31
0.75	0	2447	-2939	-416	453	454	56.88	33.74
0.80	0	2087	-2921	-174	453	454	50.86	37.70
0.85	0	1952	-2971	-97	453	454	45.52	40.24
0.90	0	1844	-2707	-45	453	454	40.53	41.19
0.95	0	1796	-2677	-27	453	454	35.36	43.10
1.00	0	1788	-2690	-18	453	454	31.41	43.35
1.05	0	1811	-2710	-8	453	454	27.31	44.28
1.10	0	1860	-2764	-4	453	454	23.41	44.56
1.15	0	1731	-2835	-1	453	454	17.31	44.30
1.20	0	2023	-2930	-0	453	454	16.32	44.93
1.25	0	2130	-3039	-0	453	454	13.12	44.86
1.30	0	2285	-3280	-0	453	454	10.34	44.81
1.35	0	2386	-3294	-0	453	454	7.33	44.92
1.40	0	2530	-3438	-0	453	454	4.79	44.95
1.45	0	2131	-3576	-0	453	454	2.41	44.97
1.50	0	1759	-3718	-0	1504	454	0.53	44.99



DETERMINATION OF CLOSING TIMEVALVE SIZE 12" VALVE CLASS 150ACTUATOR Bell & Gossett N721C-SR80-M3HWAMOUNT OF VALVE OPENING 70°DIRECTION OF FLOW No preference

## ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 7770

ACTUATOR VOLUME	<u>.72</u>	SCF	ACTUATOR YOKE RADIUS	<u>2.5</u>	IN.
ACTUATOR PRESSURE	<u>80</u>	PSIG	SOLENOID VALVE C <sub>v</sub>	<u>2.26</u>	
MEDIA	<u>Air</u>		VALVE C <sub>v</sub>	<u>494L</u>	
HYDRODYNAMIC TORQUE @ 90	<u>761</u>		SHUT OFF PRESSURE DROP	<u>45</u>	PSI
PACKING TORQUE	<u>7.7</u>	IN.LBS.	SEAL TORQUE	<u>1183</u>	IN.LBS.
STEM DIA.	<u>1.25</u>	IN.	GAGE DIA.	<u>11.703</u>	IN.
BUILDING PRESSURE	<u>3.1</u>	PSIG	dt	<u>.05</u>	SEC.

DEG.	LOCA TORQUE (IN.LBS)
10	<u>1234</u>
20	<u>1113</u>
30	<u>855</u>
40	<u>1873</u>
50	<u>2209</u>
60	<u>1940</u>
70	<u>1111</u>
80	<u>1798</u>
90	<u>5174</u>



DETERMINATION OF CLOSING TIME

12 SEC VALVE OPENING TIME DUE TO EROSION

THE VALVE OPENING IS RESTRICTED TO 70 SECS.

THE VALVE IS IN THE NON-PREFERRED DIRECTION

FEEDING SPRINGS = 6330  
ACT. VOL. = .72  
MEDIA=AIR  
PACKING TORQUE = 756  
BUILDING PRESSURE= 3.1

FED LINE, CHAIN, 3770  
ACT. YOKE RADIUS= 2.5  
VALVE Cv= 4942  
SEAL TORQUE= 1123

ACT. PRESS= 90  
HYDRO. TORQUE @ 90= 731  
0.7502 1.123

SOL. VALUE Cv= 2.25  
SHUT-OFF PRES. CRDP= 45  
0.7502 1.123

SECS.	10	20	30	40	50	60	70	80	90
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LOCA TORQUE	1234	1113	855	1873	2209	1940	1111	1779	5174
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TIME	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	TORQUE	ANGLE
sec	torque to open	spring	flow	packing & seal	spring	spring	spring	degrees
0.00	6097	8475	-3488	-99	756	454	70.00	
0.10	4196	6564	-3488	-99	756	454	70.00	
0.20	3043	5423	-3488	-99	756	454	70.00	
0.30	2259	4637	-3488	-99	756	454	70.00	
0.40	1687	4065	-3488	-99	756	454	70.00	
0.50	1247	3625	-3488	-99	756	454	70.00	
0.60	898	3276	-3488	-99	756	454	70.00	
0.70	612	2990	-3488	-99	756	454	70.00	
0.80	374	2742	-3488	-99	756	454	70.00	
0.90	173	2551	-3488	-99	756	454	70.00	
1.00	0	2372	-3488	-99	756	454	70.00	
1.10	0	2227	-3488	-99	756	454	70.00	
1.20	0	1541	-3072	623	453	454	61.27	
1.30	0	1078	-2975	888	453	454	54.08	
1.40	0	880	-2794	933	453	454	48.32	
1.50	0	1050	-2750	792	453	454	43.95	
1.60	0	1271	-2690	510	453	454	38.50	
1.70	0	704	-2373	-134	452	454	32.15	
1.80	0	2042	-2743	-186	453	454	23.45	
1.90	0	2087	-2950	-45	453	454	15.59	
2.00	0	2117	-3171	-45	453	454	0.00	
2.10	0	3274	-3420	-704	453	454	4.10	



APPENDIX E

Comparison of Actual to Calculated  
Closing Times



DETERMINATION OF CLOSING TIME

VALVE SIZE 14" VALVE CLASS 150

ACTUATOR Bell's N721 C-SR8D-M3HW

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW —

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 7770

ACTUATOR VOLUME .72 SCF ACTUATOR YORE RADIUS 2.5 IN.

ACTUATOR PRESSURE 50 PSIG SOLENOID VALVE C<sub>v</sub> 2.26

MEDIA   VALVE C<sub>v</sub>  

HYDRODYNAMIC TORQUE @ 90   SHUT OFF PRESSURE DROP   PSI

PACKING TORQUE 832 IN.LBS. SEAL TORQUE 1454 IN.LBS.

STEM DIA. 1.375 IN. GAGE DIA. 12.974 IN.

BUILDING PRESSURE 0 PSIG dt 0.1 SEC.

DEG.	DENSITY (LBS/FT. <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10			
20			
30			
40			
50			
60			
70			
80			
90			



DETERMINATION OF DELAYING TIME

THERE IS NO FLOW

Spring setting 5930  
ACT. VOL. = .13  
PACKING TORQUE = 832  
BUILDING PRESSURE = 0

Spring setting 3770  
ACT. YOKE RADIUS = 0.5  
SEAL TORQUE = 1464

ACT. PRESS = 30  
System = 1.375

SOL. VALVE CV = 2.24  
Dome = 11.774

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	8424	13517	-5924	0	832	0	90.00	0.00
0.10	5254	10347	-5924	0	832	0	90.00	0.00
0.20	3373	9189	-5924	0	832	0	90.00	0.00
0.30	2146	7239	-5924	0	832	0	90.00	0.00
0.40	1237	6330	-5924	0	832	0	90.00	0.00
0.50	371	5334	-5924	0	832	0	90.00	0.00
0.60	0	5084	-5924	0	832	0	90.00	0.00
0.70	0	4017	-4517	0	499	0	81.52	0.00
0.80	0	3043	-3942	0	499	0	70.94	0.00
0.90	0	2498	-2997	0	499	0	58.78	0.00
1.00	0	2279	-2779	0	499	0	46.80	0.00
1.10	0	2193	-2976	0	499	0	35.19	0.00
1.20	0	2241	-2741	0	499	0	24.29	0.00
1.30	0	2437	-2937	0	499	0	16.10	0.00
1.40	0	2583	-3283	0	499	0	8.79	0.00
1.50	0	2689	-3565	0	876	0	2.79	0.00



## POSI-SEAL INTERNATIONAL, INC.

## VALVE ASSEMBLY CYCLE TEST REPORT

PSI VALVE SERIAL NO.		TRAVELER NO.	
19157-034		83-19157-03-0100	
CUSTOMER	PURCHASE ORDER NO.	ITEM	TAG NO.
Stone + Webster	NMP2-P304D		ZCPSTADY104

OPERATOR TYPE	MANUFACTURER	SERIAL NO.
N721C-SR80-M3HW	BETTIS	83-9021-3

ACCESSORIES: As listed per spec. Sheet.

CYCLE TEST REQUIREMENTS PER SPECIFICATION: 19157 T-5, REV.B

## TEST CONDITIONS

- Each valve shall be cycle tested with the specific actuator which will be shipped with that particular valve.
- This test shall be performed after hydrostatic testing is completed and without further adjustment to packing.
- Each valve shall be cycled, open and closed two (2) times with its actuator. The valve shall also be cycled once with the maximum working differential pressure applied (= 150 PSIG). The time to open and close the valve shall not exceed three (3) minutes for valves with manual gear actuators.
- During the cycle test, there shall be no binding or malfunctions.

## TEST RESULTS

1. Failure Mode: F/c
2. Closed to Open:
- |                                                  |                                             |
|--------------------------------------------------|---------------------------------------------|
| First time: <u>1.9</u> sec. (w/actuator)         | Second time: <u>1.8</u> sec. (w/actuator)   |
| Third time: <u>1.7</u> sec. (w/ <u>150</u> PSIG) | Fourth time: <u>60</u> sec. (Man. override) |
- Open to Closed:
- |                                                  |                                             |
|--------------------------------------------------|---------------------------------------------|
| First time: <u>1.7</u> sec. (w/actuator)         | Second time: <u>1.7</u> sec. (w/actuator)   |
| Third time: <u>1.7</u> sec. (w/ <u>114</u> PSIG) | Fourth time: <u>60</u> sec. (Man. override) |
3. During the cycle test, there shall be no binding or malfunctions.
4. The cycle test was performed and completed satisfactorily in accordance with all requirements per PSI Specification No. 19157-T5, Rev.B

NIAGARA MOHAWK POWER CORP  
NINE MILE POINT NUC STA UNIT 2  
P.O. BOX NMP2-P3040 JC AC 12177  
BUTTERFLY VALVES - CATEGORY I  
PAGE 56 TAGZCPSTADY104.....

GAGE #1091

TESTED BY <u>F. ROSE</u>	DATE <u>7/8/83</u>	INSPECTED BY <u>Stipek, Duran</u>	DATE <u>7/8/83</u>
WITNESSED BY <u>J. G. Donovan SWEC PQA</u>	DATE <u>7-8-83</u>	AUTHORIZED INSPECTOR	DATE



DETERMINATION OF CLOSING TIME

VALVE SIZE 12" VALVE CLASS 150

ACTUATOR Bell & Gossett N721C-SR80-M34W

AMOUNT OF VALVE OPENING 90°

DIRECTION OF FLOW -

ACTUATOR TORQUES (IN.LBS)

SPRING BEGINNING 5930 SPRING ENDING 3770

ACTUATOR VOLUME .72 SCF ACTUATOR YORE RADIUS 2.5 IN.

ACTUATOR PRESSURE 80 PSIG SOLENOID VALVE C<sub>v</sub> 2.26

MEDIA  VALVE C<sub>v</sub>

HYDRODYNAMIC TORQUE @ 90  SHUT OFF PRESSURE DROP  PSI

PACKING TORQUE 750 IN.LBS. SEAL TORQUE 1183 IN.LBS.

STEM DIA. .125 IN. GAGE DIA. 11703 IN.

BUILDING PRESSURE 0 PSIG dt 0.1 SEC.

DEG.	DENSITY (LBS/FT <sup>3</sup> )	VELOCITY (FT/SEC)	PRESSURE DROP (PSI)
10	<hr/>	<hr/>	<hr/>
20	<hr/>	<hr/>	<hr/>
30	<hr/>	<hr/>	<hr/>
40	<hr/>	<hr/>	<hr/>
50	<hr/>	<hr/>	<hr/>
60	<hr/>	<hr/>	<hr/>
70	<hr/>	<hr/>	<hr/>
80	<hr/>	<hr/>	<hr/>
90	<hr/>	<hr/>	<hr/>



DETERMINATION OF VALVE SEALING AND TORQUE

THERE IS NO FLOW

Spring begin <sup>s</sup> 5930	Spring ending 3770	ACT. VOL.= .72	ACT. YOKE RADIUS= 2.5	ACT. PRESS= 20	SOL. VALVE C.= 2.26
PACKING TORQUE=.75	SEAL TORQUE= 1133			DISPEN= 1725	DENSITY=.22775
GULDING PRESSURE= 0					

TIME sec	TORQUE tend to open	TORQUE air	TORQUE spring	TORQUE flow	TORQUE packing & seal	TORQUE bearing	ANGLE degrees	DELTA P psi
0.00	8348	13517	-5924	0	756	0	90.00	0.00
0.10	5178	10347	-5924	0	756	0	90.00	0.00
0.20	3320	7487	-5924	0	753	0	90.30	0.00
0.30	2070	7239	-5924	0	756	0	90.60	0.00
0.40	1161	6330	-5924	0	756	0	90.00	0.00
0.50	466	5634	-5924	0	756	0	90.60	0.00
0.60	0	5034	-5924	0	756	0	90.00	0.00
0.70	0	4063	-4517	0	453	0	81.52	0.00
0.80	0	3980	-3933	0	453	0	70.71	0.00
0.90	0	2933	-2987	0	453	0	58.54	0.00
1.00	0	2321	-2775	0	453	0	46.24	0.00
1.10	0	2221	-2695	0	453	0	34.45	0.00
1.20	0	2300	-2753	0	453	0	24.04	0.00
1.30	0	2510	-2964	0	453	0	15.23	0.00
1.40	0	2527	-3253	0	453	0	8.94	0.00
1.50	0	2489	-3618	0	1128	0	2.02	0.00



## POSI-SEAL INTERNATIONAL, INC.

## VALVE ASSEMBLY CYCLE TEST REPORT

PSI VALVE SERIAL NO.	19157-4A	TRAVELER NO.	83-19157-04
CUSTOMER	PURCHASE ORDER NO.	ITEM	TAG NO.
Stone + Webster	NMP2-P304D		2CPSAOV107

OPERATOR TYPE	MANUFACTURER	SERIAL NO.
N721C-SR80-M3HW	BETTIS	83-9021-8

ACCESSORIES: As listed per spec. Sheet.

CYCLE TEST REQUIREMENTS PER SPECIFICATION: 19157 T-5, Rev.B

## TEST CONDITIONS

- Each valve shall be cycle tested with the specific actuator which will be shipped with that particular valve.
- This test shall be performed after hydrostatic testing is completed and without further adjustment to packing.
- Each valve shall be cycled, open and closed two (2) times with its actuator. The valve shall also be cycled once with the maximum working ~~different~~ pressure applied (= 150 PSIG). The time to open and close the valve shall not exceed three (3) minutes for valves with manual gear actuators.
- During the cycle test, there shall be no binding or malfunctions.

## TEST RESULTS



1. Failure Mode: FAIL CLOSED

2. Closed to Open:

First time: 2.1 sec. (w/actuator)

Second time: 2.0 sec. (w/actuator)

Third time: 2.2 sec. (w/ 150 PSIG)

Fourth time: 2.4 sec. (man. override)

Open to Closed:

First time: 1.7 sec. (w/actuator)

Second time: 1.7 sec. (w/actuator)

Third time: 2.0 sec. (w/ N/A PSIG)

Fourth time: 2.1 sec. (man. override)

- During the cycle test, there shall be no binding or malfunctions.
- The cycle test was performed and completed satisfactorily in accordance with all requirements per PSI Specification No. 19157-T5, Rev.B

NIAGARA MOHAWK POWER CORP  
NINE MILE POINT NUC STA UNIT 2  
P.O. NO. NMP2-P304D JO NO 12177  
BUTTERFLY VALVES - CATEGORY I  
PAGE 41 TAG 2CPSAOV107.....

Post-Seal International, Inc.  
Rts. 49 & U.S. 95  
North Stonington, Conn. 06779

I-1091

TESTED BY <i>John Robbins</i>	DATE 7-11-83	INSPECTED BY <i>Jude Bandiak</i>	DATE 7-11-83
WITNESSED BY <i>J. G. Donovan S.E.W.P.C.A.</i>	DATE 7-11-83	AUTHORIZED INSPECTOR	DATE



APPENDIX G

Seismic and LOCA Stress Analysis



### NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 14"  
 VALVE CLASS: 150  
 ACTUATOR: N721C - SR80 - M3 HW  
 CUSTOMER: Unit - 2 - Malawik  
 P.O. NO.: NMPJ2 - P304N / 12127  
 SPEC. NO.: NMP2 - P304N and Add = 1, - 2 + 3  
 REFERENCE NO.: 19157  
 ITEM NO.: 3 AOU 106

### REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-3</u>	REV.	<u>B</u>
B. BODY DWG. NO.	<u>1114-302</u>	REV.	<u>A</u>
C. DISC DWG. NO.	<u>2114-301</u>	REV.	<u>B</u>
D. STEM DWG. NO.	<u>2510-015</u>	REV.	<u>A</u>
E. PIN DWG. NO.	<u>2600-060</u>	REV.	<u>A</u>
F. BRACKET DWG. NO.	<u>8000-197</u>	REV.	<u>-</u>

### ALLOWABLE STRESSES

A. BODY	<u>SA 351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA 351 GR C70 (and H107)</u>	<u>52800</u>	PSI
C. PIN	<u>SA 351 GR C30 (and H107)</u>	<u>52800</u>	PSI
D. BRACKET	<u>CS</u>	<u>18900</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

### DESIGN CONDITIONS

PRESSURE: 45 PSI  
 TEMPERATURE: 340 DEG. F.

### VALVE TORQUES

LOCA TORQUE: 6170 Case 1A IN-LBS  
 MEDIA: Oil  
 FLOW DIRECTION: Upward

### G-LOADINGS

TRANSVERSE: 4  
 VERTICAL: 3  
 LONGITUDINAL: 3



SIZE 14' CLASS 150DIMENSIONAL DATAACTUATOR N721C-C&T0-

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTE NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{2}$ VALVE	9.438	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{2}$ VALVE	2.655	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	3.685	X3
HEIGHT BRACKET	6	X4
HEIGHT VALVE NECK	1.375	X5
ACTUATOR WEIGHT	21.9	W1
BRACKET WEIGHT	2.7	W2
DISC WEIGHT	61	W4
THICKNESS OF BRACKET LOWER PLATE	.575	T1
WIDTH OF BRACKET	5	T2
WIDTH OF VALVE NECK	7	T3
THICKNESS OF VALVE NECK	3	T4
THICKNESS OF BRACKET SIDE PLATES	.75	T9
THICKNESS OF BRACKET TOP PLATE	.625	T0
VALVE NECK O.D.	0	D0
PACKING BORE I.D.	2.125	E5
STEM DIA.	1.375	D1
GAGE DIA. OF DISC	13.974	D
WIDTH SMALL DIA. BACK OF DISC	1.906	E1
WIDTH LARGE DIA. OF DISC	1.913	E2
THRUST WASHER THICKNESS	1.316	L2
DIST. $\frac{1}{2}$ STEM TO FRONT OF DISC	1.604	Y2
NO. OF ACTUATOR BOLTS	4	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	.1415	A1
DBC OF ACTUATOR BOLTS	4.5	X6
NO. OF BRACKET/VALVE BOLTS	4	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	.1416	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	5	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	2	X8
LENGTH OF BRACKET	9.75	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	0	R5
DIA. OF VALVE BODY BOLT HOLES	0	R6
% TORQUE ON DISC PIN	6.5	%
DISC PIN DIA.	4.19	D5
VALVE BODY O.D.	2.1	D1
VALVE BODY WATERWAY DIA.	13.312	D7
ADJACENT PIPING O.D.	14	R8
ADJACENT PIPING I.D.	13.126	R9
MAXIMUM PIPING BENDING MOMENT	N/A	M4
NO. OF BODY BOLTS	71	N3
DBC OF BODY BOLTS	1	X0
ROOT AREA OF BODY BOLTS	1	A4
LENGTH ACROSS GUSSETS	0	L
THICKNESS OF GUSSETS	0	T
DIA. OF FLANGE BOSSES	0	B
MODULUS OF ELASTICITY	30,000,000	E



## FEDERAL-MOGUL VALVE DIVISION, INC.

## 14 CLASS 150 VALVE ASSEMBLY

CUSTOMER: NIAGARA MOGUL  
PROJ. NUMBER: 19157-3 REV. C  
SPEC. NO.: NMPC-P/304D  
REF. NO.: 19157  
ITEM NO.: 5

## REFERENCE DWGS.

A. ASSY DWG. NO.: 19157-3 REV. C  
B. BODY DWG. NO.: 1114-502 REV. A  
C. DISC DWG. NO.: 2114-301 REV. B  
D. STEM DWG. NO.: 2610-013 REV. A  
E. PIN DWG. NO.: 2600-060 REV. A  
F. BRACKET DWG. NO.: 8000-197 REV. -

## ALLOWABLE STRESSES (PSI)

A.BODY: 23400  
B.STEM: 52900  
C.PIN: 52800  
D.BRACKET: 13900  
E.BOLTING: 37500

DESIGN CONDITIONS  
PRESSURE(PSIG)= 45

TEMPERATURE = 77° F 24° C

## G LOADINGS

LOCAL FORCE= 3470

TRANSVERSE= 4

MEDIA=AIR

VERTICAL= 3

FLOW DIRECTION=PREFERRED

LONGITUDINAL= 3

## DIMENSIONAL DATA

X1= 8.438	X2= 3.688	X3= 3.688	X4= 5	X5= 1.375	W1= 219	W2= 27
W4=.31	T1=.373	T2=.3	T3=.2	T4=.3	E1=.73	E2=.325
d3= 0	D1= 2.125	D2= 1.375	D3= 12.974	E1= 1.906	E2=.313	
L2=.316	Y2= 1.604	N1= 4	A1=.1416	X6= 4.5	N2= 4	
A2=.2478	X7=.5	X8=.5	T5=.75	R3=.0		
Z=.65	d5=.493	d1= 21	R7= 13.312	R8=.14	R9= 13.125	
L= 0	T= 0	B= 0	E= 30000000			

## NATURAL FREQUENCIES (HZ.)

## ACTUATOR BOLT STRESSES

LONGITUDINAL(Z) ACT./VALVE= 95 VS. 33HZ.

SHEAR= 9901 PSI

VERTICAL(Y) ACT./VALVE= 67.3 VS. 33HZ.

TENSILE= 3471 PSI

TRANSVERSE(X) ACT./VALVE= 130 VS.33HZ.

COMBINED= 15019 PSI VS.ALLOW.= 37500

LATERAL DISC/STEM= 604 VS.33HZ.

SHEAR= 3315 PSI

SHEAR= 638 PSI

TENSILE= 17410 PSI

TENSILE= 3357 PSI

COMBINED= 20400 PSI VS.ALLOW= 37500

COMBINED= 3765 PSI VS.ALLOW= 18700

## VALVE NECK STRESSES

## STEM STRESSES

SHEAR= 917 PSI

SHEAR= 12087 PSI

TENSILE= 1234 PSI

TENSILE= 4460 PSI

COMBINED= 1722 PSI VS.ALLOW= 33400

COMBINED= 17622 PSI VS.ALLOW= 50200

## DISC PIN STRESS

## SECTION MODULUS

SHEAR= 14800 PSI VS.ALLOW= 31680

VALVE= 761.36 IN43

PIPE= 61.22 IN43

## ACTUATOR DEFLECTIONS

## BODY BOLTING

LONGITUDINAL= 3.83100000E-03 INCHES

NOT APPLICABLE

VERTICAL= 3.30000000E-05 INCHES

TRANSVERSE= 2.19030000E-03 INCHES

SIGNED. *[Signature]* ..... DATED. *5/22/87* .....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 14"  
VALVE CLASS: 150  
ACTUATOR: N721C - SRKO - M3 H/W  
CUSTOMER: Niagara Mohawk  
P.O. NO.: NMP2- P304N / 12177  
SPEC. NO.: NMP2- P304N and Add #1, #2 & #3  
REFERENCE NO.: 19157  
ITEM NO.: 3 ADV 104

REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-3</u>	REV.	<u>B</u>
B. BODY DWG. NO.	<u>1114-302</u>	REV.	<u>A</u>
C. DISC DWG. NO.	<u>2114-301</u>	REV.	<u>B</u>
D. STEM DWG. NO.	<u>2510-015</u>	REV.	<u>A</u>
E. PIN DWG. NO.	<u>2600-060</u>	REV.	<u>A</u>
F. BRACKET DWG. NO.	<u>8000-197</u>	REV.	<u>-</u>

ALLOWABLE STRESSES

A. BODY	<u>SA 351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA 351 GR C10 Cond H107J</u>	<u>52300</u>	PSI
C. PIN	<u>SA 351 GR C30 Cond H107J</u>	<u>52300</u>	PSI
D. BRACKET	<u>CS</u>	<u>18900</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 7339 Case 1B IN-LBS  
MEDIA: Air  
FLOW DIRECTION: Non preferred

G-LOADINGS

TRANSVERSE: 3  
VERTICAL: 4  
LONGITUDINAL: 3



SIZE 14' CLASS 150DIMENSIONAL DATAACTUATOR N721C-CR80-1

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	9.438	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	2.689	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	3.699	X3
HEIGHT BRACKET	6	X4
HEIGHT VALVE NECK	1.375	X5
ACTUATOR WEIGHT	219	W1
BRACKET WEIGHT	27	W2
DISC WEIGHT	61	W4
THICKNESS OF BRACKET LOWER PLATE	.575	T1
WIDTH OF BRACKET	5	T2
WIDTH OF VALVE NECK	7	T3
THICKNESS OF VALVE NECK	3	T4
THICKNESS OF BRACKET SIDE PLATES	.75	T9
THICKNESS OF BRACKET TOP PLATE	.625	T0
VALVE NECK O.D.	0	G3
PACKING BORE I.D.	2.125	D1
STEM DIA.	1.375	D1
GAGE DIA. OF DISC	13.974	D
WIDTH SMALL DIA. BACK OF DISC	1.906	E1
WIDTH LARGE DIA. OF DISC	1.913	E2
THRUST WASHER THICKNESS	.316	L2
DIST. $\frac{1}{4}$ STEM TO FRONT OF DISC	1.604	Y2
NO. OF ACTUATOR BOLTS	4	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	.1413	A1
DBC OF ACTUATOR BOLTS	4.5	X6
NO. OF BRACKET/VALVE BOLTS	4	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	.1416	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	5	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	2	X8
LENGTH OF BRACKET	9.75	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	0	R5
DIA. OF VALVE BODY BOLT HOLES	0	R6
% TORQUE ON DISC PIN	65	T7
DISC PIN DIA.	.419	D5
VALVE BODY O.D.	21	D8
VALVE BODY WATERWAY DIA.	13.312	R7
ADJACENT PIPING O.D.	14	R8
ADJACENT PIPING I.D.	13.126	R9
MAXIMUM PIPING BENDING MOMENT	N/A	M4
NO. OF BODY BOLTS	1	N3
DBC OF BODY BOLTS	1	X0
ROOT AREA OF BODY BOLTS	1	A4
LENGTH ACROSS GUSSETS	0	L
THICKNESS OF GUSSETS	0	T
DIA. OF FLANGE BOSSES	0	B
MODULUS OF ELASTICITY	30,000,000	E



## POST-SHOCK INSTRUMENTATION, INC.

## 14 CLASS 150 VALVE ASSEMBLY

WCB PRESSURE VESSEL

CUSTOMER: NAIARA MOHAUK

REF. NO.: 19157

SPEC. NO.: NMP2-P; 3040

REF. NO.: 19157

ITEM NO.: 73

## REFERENCE DWGS.

A. ASSEMBLY DWG. NO.: 19157-3 REV.B  
 B. BODY DWG. NO.: 1114-302 REV.A  
 C. DISC DWG. NO.: 2114-301 REV.B  
 D. STEM DWG. NO.: 12510-315 REV.A  
 E. PIN DWG. NO.: 12600-060 REV.A  
 F. BRACKET DWG. NO.: 3000-197 REV.-

## ALLOWABLE STRESSES (PSI)

A. BODY: 23400  
 B. STEM: 52900  
 C. PIN: 53800  
 D. BRACKET: 18900  
 E. BOLTING: 37500

## DESIGN CONDITIONS

PRESSURE(PSIG)= 45

TEMPERATURE(F)= 340

## G LOADINGS

LOAD TORQUE= 7339

MEDIA=AIR

FLOW DIRECTION=NONPREFERRED

TRANSVERSE= 3

VERTICAL= 4

LONGITUDINAL= 3

## DIMENSIONAL DATA

X1= 8.438	X2= 2.588	X3= 3.638	X4= 6	X5= 1.375	W1= 219	W2= 27
Y1= .31	Y2= .375	T1= 5	T3= 7	T4= 3	T9= .75	T0= .325
d3= 0	D1= 2.125	D1= 1.375	D= 12.974	E1= 1.906	E2= .813	
L2= .316	Y2= 1.604	N1= 4	A1= .1416	X6= 4.5	N2= 4	
R1= .1416	X2= 3	N2= 2	A2= .775	R5= .5	R3= .5	
Z= .65	dp= .498	d1= 21	R7= 13.312	R8= 14	R9= 13.126	
L= 0	T= 0	G= 0	E= 30000000			

## NATURAL FREQUENCIES (HZ.)

LONGITUDINAL(Z) ACT./VALVE= 85 VS. 33HZ.

VERTICAL(Y) ACT./VALVE= 110 VS. 33HZ.

TRANSVERSE(X) ACT./VALVE= 130 VS. 33HZ.

LATERAL DISC/STEM= 604 VS. 33HZ.

## ACTUATOR BOLT STRESSES

SHEAR= 10372 PSI

TENSILE= 19314 PSI

COMBINED= 17018 PSI VS. ALLOW.= 37500

## BRACKET BOLT STRESSES

SHEAR= 8362 PSI

TENSILE= 19314 PSI

COMBINED= 21557 PSI VS. ALLOW= 37500

## BRACKET STRESSES

SHEAR= 631 PSI

TENSILE= 3987 PSI

COMBINED= 3983 PSI VS. ALLOW= 19900

## VALVE NECK STRESSES

SHEAR= 969 PSI

TENSILE= 1284 PSI

COMBINED= 1305 PSI VS. ALLOW= 23400

## STEM STRESSES

SHEAR= 14378 PSI

TENSILE= 4427 PSI

COMBINED= 15731 PSI VS. ALLOW= 62600

## DISC PIN STRESS

SHEAR= 17314 PSI VS. ALLOW= 31680

## SECTION MODULUS

VALVE= 762.38 IN13

PIPING= 61.22 IN13

## ACTUATOR DEFLECTIONS

LONGITUDINAL= 3.83100000E-03 INCHES

VERTICAL= 1.11000000E-04 INCHES

TRANSVERSE= 1.20000000E-03 INCHES

## BODY BOLTING

NOT APPLICABLE

SIGNED.. *John L. Lutz* ..... DATED.. 6/1/87 .....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 14"  
VALVE CLASS: 150  
ACTUATOR: N721C - SR80 - M3 HWI  
CUSTOMER: Niagara Mohawk  
P.O. NO.: NMP2 - P304N / 12127  
SPEC. NO.: NMP2 - P304N and Add -1, -2, +3  
REFERENCE NO.: 19157  
ITEM NO.: 3 AOV 108

REFERENCE DWGS.

A.. ASS'Y DWG. NO.	<u>19157-3</u>	REV. <u>B</u>
B. BODY DWG. NO.	<u>1114-302</u>	REV. <u>A</u>
C. DISC DWG. NO.	<u>2114-301</u>	REV. <u>B</u>
D. STEM DWG. NO.	<u>2510-015</u>	REV. <u>A</u>
E. PIN DWG. NO.	<u>2600-060</u>	REV. <u>A</u>
F. BRACKET DWG. NO.	<u>8000-197</u>	REV. <u>-</u>

ALLOWABLE STRESSES

A. BODY	<u>SA 351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA 351 GR C10 Cold H1077</u>	<u>52800</u>	PSI
C. PIN	<u>SA 351 GR G30 Cold H1077</u>	<u>51800</u>	PSI
D. BRACKET	<u>CS</u>	<u>18900</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 5848 Case 2A IN-LBS  
MEDIA: Air  
FLOW DIRECTION: Preferred

G-LOADINGS

TRANSVERSE: 4  
VERTICAL: 3  
LONGITUDINAL: 3



SIZE 14' CLASS 150DIMENSIONAL DATAACTUATOR N721C-SK90-

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	X1	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	X2	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	X3	X3
HEIGHT BRACKET	X4	X4
HEIGHT VALVE NECK	X5	X5
ACTUATOR WEIGHT	W1	W4
BRACKET WEIGHT	W2	W5
DISC WEIGHT	W4	W3
THICKNESS OF BRACKET LOWER PLATE	T1	T1
WIDTH OF BRACKET	T2	T2
WIDTH OF VALVE NECK	T3	T3
THICKNESS OF VALVE NECK	T4	T4
THICKNESS OF BRACKET SIDE PLATES	T9	T9
THICKNESS OF BRACKET TOP PLATE	T0	T0
VALVE NECK O.D.	d3	D0
PACKING BORE I.D.	Di	D5
STEM DIA.	D1	D1
GAGE DIA. OF DISC	D	D
WIDTH SMALL DIA. BACK OF DISC	E1	E1
WIDTH LARGE DIA. OF DISC	E2	E2
THRUST WASHER THICKNESS	L2	L2
DIST. $\angle$ STEM TO FRONT OF DISC	Y2	Y2
NO. OF ACTUATOR BOLTS	N1	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	A1	A1
DBC OF ACTUATOR BOLTS	X6	X6
NO. OF BRACKET/VALVE BOLTS	N2	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	A2	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	X7	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	X8	X8
LENGTH OF BRACKET	T5	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	R5	R5
DIA. OF VALVE BODY BOLT HOLES	R6	R6
% TORQUE ON DISC PIN	S	T7
DISC PIN DIA.	d5	D5
VALVE BODY O.D.	d1	D8
VALVE BODY WATERWAY DIA.	R7	R7
ADJACENT PIPING O.D.	R8	R8
ADJACENT PIPING I.D.	R9	R9
MAXIMUM PIPING BENDING MOMENT	M4	M4
NO. OF BODY BOLTS	N3	N3
DBC OF BODY BOLTS	X0	X0
ROOT AREA OF BODY BOLTS	A4	A4
LENGTH ACROSS GUSSETS	L	L
THICKNESS OF GUSSETS	T	T
DIA. OF FLANGE BOSSES	B	B
MODULUS OF ELASTICITY	E	E
	30,000,000	



## FISI-SEAL INTERNATIONAL, INC.

14 CLASS 150 VALVE ASSEMBLY

CUSTOMER: NIAGARA MACHINERY  
 P.O. NO.: NMP2-PTC-01-0000000000000000  
 SPEC. NO.: NMP2-P; 3040  
 REF. NO.: 19157  
 ITEM: N/A

REFERENCE DWGS.  
 A.BRASS TUBE DWG. NO.: 19117-3 REV. 3  
 B.BODY DWG. NO.: 1114-302 REV. A  
 C.DISC DWG. NO.: 2114-301 REV. B  
 D.STEM DWG. NO.: 2510-015 REV. A  
 E.PIN DWG. NO.: 2600-050 REV. A  
 F.BRACKET DWG. NO.: 8000-197 REV. -

ALLOWABLE STRESSES (PSI)  
 A.BRASS: 23400  
 B.STEM: 52900  
 C.PIN: 52900  
 D.BRACKET: 13700  
 E.BOLTING: 37500

DESIGN CONDITIONS  
 PRESSURE(PSIC)= 45  
 TEMPERATURE= 77° + 34°

## G LOADINGS

LOAD TORQUE= 5848  
 MEDIA=AIR  
 FLOW DIRECTION=PREFERRED

TRANVERSE= 4  
 VERTICAL= 3  
 LONGITUDINAL= 3

## DIMENSIONAL DATA

X1= 8.438	X2= 2.689	X3= 3.689	X4= 6	X5= 1.375	W1= 219	W2= 27
W1=.51	T1=.375	T2= 3	T3= 7	T4= 3	T5=.75	T6=.1525
d3= 0	D1= 2.125	D1= 1.375	D= 12.974	E1= 1.906	E2=.813	
L2=.315	Y2= 1.604	N1= 4	A1=.1416	X5= 4.5	N2= 4	
Z=.413	X7=.5	X8= 2	T5=.75	R5=.0	R6=.1	
Z= 65	dp=.498	di= 21	R7= 13.312	R9= 14	R9= 13.125	
L= 0	T= 0	G= 0	E= 30000000			

NATURAL FREQUENCIES (HZ.)  
 LONGITUDINAL(Z) ACT./VALVE= 35 VS. 33HZ.  
 VERTICAL(Y) ACT./VALVE= 37 VS. 33HZ.  
 TRANSVERSE(X) ACT./VALVE= 130 VS. 33HZ.  
 LATERAL DISC/STEM= 304 VS. 33HZ.

ACTUATOR BOLT STRESSES  
 SHEAR= 9650 PSI  
 TENSILE= 3574 PSI  
 COMBINED= 14738 PSI VS ALLOW.= 37500

BRACKET BOLT STRESSES  
 SHEAR= 9107 PSI  
 TENSILE= 42010 PSI  
 COMBINED= 20255 PSI VS ALLOW.= 37500

BRACKET STRESSES  
 SHEAR= 629 PSI  
 TENSILE= 3574 PSI  
 COMBINED= 3701 PSI VS ALLOW.= 18900

VALVE NECK STRESSES  
 SHEAR= 396 PSI  
 TENSILE= 1234 PSI  
 COMBINED= 1705 PSI VS ALLOW.= 23400

STEM STRESSES  
 SHEAR= 11456 PSI  
 TENSILE= 4460 PSI  
 COMBINED= 13900 PSI VS ALLOW.= 52900

DISC PIN STRESS  
 SHEAR= 14035 PSI VS ALLOW.= 31830

SECTION MODULUS  
 VALVE= 755.38 IN43  
 PIPING= 61.22 IN43

ACTUATOR DEFLECTIONS  
 LONGITUDINAL= 3.83100000E-03 INCHES  
 VERTICAL= 8.30000000E-05 INCHES  
 TRANSVERSE= 2.10000000E-03 INCHES

BODY BOLTING

NOT APPLICABLE

SIGNED... *[Signature]* ..... DATED... *[Signature]* .....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 14"  
VALVE CLASS: 150  
ACTUATOR: N721C - SR80 - M3 H4W  
CUSTOMER: Via Jaca Milbank  
P.O. NO.: NMPJ2 - P304 N / 12177  
SPEC. NO.: NMPZ - P304 N and Add #1, #2, #3  
REFERENCE NO.: 19157  
ITEM NO.: 3 ADU 110

REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-3</u>	REV.	<u>B</u>
B. BODY DWG. NO.	<u>1114-302</u>	REV.	<u>A</u>
C. DISC DWG. NO.	<u>2114-701</u>	REV.	<u>B</u>
D. STEM DWG. NO.	<u>2510-015</u>	REV.	<u>A</u>
E. PIN DWG. NO.	<u>2600-060</u>	REV.	<u>A</u>
F. BRACKET DWG. NO.	<u>8000-197</u>	REV.	<u>-</u>

ALLOWABLE STRESSES

A. BODY	<u>SA 351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA 351 GR C70 Cond H107T</u>	<u>52800</u>	PSI
C. PIN	<u>SA 371 GR 630 Cond H107T</u>	<u>52800</u>	PSI
D. BRACKET	<u>CS</u>	<u>18400</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 9584 C<sub>o</sub>c 2B IN-LBS  
MEDIA: Air  
FLOW DIRECTION: Preferred

G-LOADINGS

TRANSVERSE: 3  
VERTICAL: 3  
LONGITUDINAL: 4



SIZE 14" CLASS 150DIMENSIONAL DATAACTUATOR N721C-SK80-A

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO 4" VALVE	9.438	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO 4" VALVE	2.655	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	3.689	X3
HEIGHT BRACKET	6	X4
HEIGHT VALVE NECK	1.325	X5
ACTUATOR WEIGHT	219	W1
BRACKET WEIGHT	27	W2
DISC WEIGHT	61	W4
THICKNESS OF BRACKET LOWER PLATE	.875	T1
WIDTH OF BRACKET	5	T2
WIDTH OF VALVE NECK	7	T3
THICKNESS OF VALVE NECK	3	T4
THICKNESS OF BRACKET SIDE PLATES	.75	T9
THICKNESS OF BRACKET TOP PLATE	.625	T0
VALVE NECK O.D.	0	d3
PACKING BORE I.D.	2.125	D1
STEM DIA.	1.375	D1
GAGE DIA. OF DISC	12.974	D
WIDTH SMALL DIA. BACK OF DISC	1.906	E1
WIDTH LARGE DIA. OF DISC	.913	E2
THRUST WASHER THICKNESS	.316	L2
DIST. 4" STEM TO FRONT OF DISC	1.604	Y2
NO. OF ACTUATOR BOLTS	4	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	.1418	A1
DEC OF ACTUATOR BOLTS	.45	X6
NO. OF BRACKET/VALVE BOLTS	4	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	.1416	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	5	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	2	X8
LENGTH OF BRACKET	9.75	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	0	R5
DIA. OF VALVE BODY BOLT HOLES	0	R6
% TORQUE ON DISC PIN	.65	T7
DISC PIN DIA.	.418	D5
VALVE BODY O.D.	.21	D8
VALVE BODY WATERWAY DIA.	13.312	R7
ADJACENT PIPING O.D.	.14	R8
ADJACENT PIPING I.D.	13.126	R9
MAXIMUM PIPING BENDING MOMENT	N/A	M4
NO. OF BODY BOLTS	1	N3
DEC OF BODY BOLTS	1	X0
ROOT AREA OF BODY BOLTS	1	A4
LENGTH ACROSS GUSSETS	0	L
THICKNESS OF GUSSETS	0	T
DIA. OF FLANGE BOSSES	0	B
MODULUS OF ELASTICITY	30,000,000	E



FIRST-SEAL INTERNATIONAL, INC.  
NUMBER 150 VALVE ASSEMBLY

14 CLASS 150 VALVE ASSEMBLY

CUSTOMER: NINGARA MOHAWK  
SPEC. NO.: NMF2-P; 3040  
REF. NO.: 119157  
ITEM NO.: 3

REFERENCE DUGS.

A. ASSY DWG. NO.: 1114-307 REV. S  
B. BODY DWG. NO.: 1114-302 REV. A  
C. DISC DWG. NO.: 1114-301 REV. S  
D. STEM DWG. NO.: 1114-308 REV. A  
E. PIN DWG. NO.: 2600-060 REV. A  
F. BRACKET DWG. NO. 9000-197 REV. -

ALLOWABLE STRESSES (PSI)

A. SCREW: 34000  
B. STEM: 52800  
C. PIN: 51800  
D. BRACKET: 10900  
E. BOLTING: 37500

DESIGN CONDITIONS

PRESSURE (PSIG) = 45

TEMPERATURE (F) = 340

C LOADINGS

LOAD TORQUE = 7534

MEDIA = AIR

FLOW DIRECTION = PREFERRED

TRANSVERSE = 3

VERTICAL = 3

LONGITUDINAL = 4

DIMENSIONAL DATA

X1 = 8.438	X2 = 2.688	X3 = 3.688	X4 = 6	X5 = 1.375	W1 = 219	W2 = 27
Z1 = .31	Z2 = .375	Z3 = 5	Z4 = 7	Z5 = 3	Z6 = .75	Z7 = .75
D1 = 0	D2 = 2.125	D3 = 1.375	D4 = 12.974	D5 = 1.706	D6 = .813	D7 = .813
L1 = .316	Y1 = 1.604	N1 = 4	A1 = .1413	X6 = 4.5	N2 = 4	N3 = 4
Z1 = .1413	X2 = 3	X3 = 2	Z5 = 9.75	R5 = 0	R6 = 0	R7 = 0
Z2 = .65	dp = .498	di = 21	R7 = 13.312	R8 = 14	R9 = 13.126	R10 = 13.126
L1 = 0	T = 0	B = 0	E = 30000000			

NATURAL FREQUENCIES (HZ.)  
LONGITUDINAL (Z) ACT./VALVE = 85 VS. 33HZ.  
VERTICAL (Y) ACT./VALVE = 87 VS. 33HZ.  
TRANSVERSE (X) ACT./VALVE = 130 VS. 33HZ.  
LATERAL DISC/STEM = 604 VS. 33HZ.

ACTUATOR BOLT STRESSES

SHEAR = 13259 PSI

TENSILE = 34947 PSI

COMBINED = 18168 PSI VS. ALLOW. = 37500

BRACKET BOLT STRESSES

SHEAR = 10333 PSI

TENSILE = 47937 PSI

COMBINED = 34240 PSI VS. ALLOW. = 37500

BRACKET STRESSES

SHEAR = 782 PSI

TENSILE = 47937 PSI

COMBINED = 5105 PSI VS. ALLOW. = 18900

VALVE NECK STRESSES

SHEAR = 1261 PSI

TENSILE = 1431 PSI

COMBINED = 2188 PSI VS. ALLOW. = 23400

STEM STRESSES

SHEAR = 18774 PSI

TENSILE = 4460 PSI

COMBINED = 2133 PSI VS. ALLOW. = 32200

DISC PIN STRESS

SHEAR = 23001 PSI VS. ALLOW. = 31580

SECTION MODULUS

VALVE = 781.89 IN<sup>3</sup>

PIPING = 61.22 IN<sup>3</sup>

ACTUATOR DEFLECTIONS

LONGITUDINAL = 5.1080000E-03 INCHES

VERTICAL = 8.3000000E-05 INCHES

TRANSVERSE = 1.3000000E-03 INCHES

BODY BOLTING

NOT APPLICABLE

SIGNED... *[Signature]* ..... DATED... *4/1/74* .....



6



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: N761C - SR80 - M3HW  
CUSTOMER: Niagara Mohawk  
P.O. NO.: NMPZ-P304D-12177  
SPEC. NO.: NMPZ-P304 D + Add w/ L, R, f + 3  
REFERENCE NO.: 19157  
ITEM NO.: 4 AOU 107

REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-4</u>	REV.	<u>A</u>
B. BODY DWG. NO.	<u>1113-301</u>	REV.	<u>A</u>
C. DISC DWG. NO.	<u>2112-301</u>	REV.	<u>A</u>
D. STEM DWG. NO.	<u>2510-013</u>	REV.	<u>A</u>
E. PIN DWG. NO.	<u>2600-060</u>	REV.	<u>A</u>
F. BRACKET DWG. NO.	<u>8000-199</u>	REV.	<u>A</u>

ALLOWABLE STRESSES

A. BODY	<u>SA351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA514 GR 630 Card H1075</u>	<u>52800</u>	PSI
C. PIN	<u>SASG4 GR 630 Card H1075</u>	<u>51500</u>	PSI
D. BRACKET	<u>CS</u>	<u>18500</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 3998 Case 3A IN-LBS  
MEDIA: Air  
FLOW DIRECTION: Upward

G-LOADINGS

TRANSVERSE: 3  
VERTICAL: 4  
LONGITUDINAL: 3



SIZE 12' CLASS 150DIMENSIONAL DATAACTUATOR 1721C-3A80-M3HL

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	X1	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	X2	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	X3	X3
HEIGHT BRACKET	X4	X4
HEIGHT VALVE NECK	X5	X5
ACTUATOR WEIGHT	W1	W4
BRACKET WEIGHT	W2	W5
DISC WEIGHT	W4	W3
THICKNESS OF BRACKET LOWER PLATE	T1	T1
WIDTH OF BRACKET	T2	T2
WIDTH OF VALVE NECK	T3	T3
THICKNESS OF VALVE NECK	T4	T4
THICKNESS OF BRACKET SIDE PLATES	T9	T9
THICKNESS OF BRACKET TOP PLATE	T0	T0
VALVE NECK O.D.	D3	D0
PACKING BORE I.D.	D1	B5
STEM DIA.	D1	D1
GAGE DIA. OF DISC	D	D
WIDTH SMALL DIA. BACK OF DISC	E1	E1
WIDTH LARGE DIA. OF DISC	E2	E2
THRUST WASHER THICKNESS	L2	L2
DIST. $\frac{1}{4}$ STEM TO FRONT OF DISC	Y2	Y2
NO. OF ACTUATOR BOLTS	N1	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	A1	A1
DBC OF ACTUATOR BOLTS	X6	X6
NO. OF BRACKET/VALVE BOLTS	N2	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	R2	R2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	X7	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	X8	X8
LENGTH OF BRACKET	T5	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	R5	R5
DIA. OF VALVE BODY BOLT HOLES	R6	R6
% TORQUE ON DISC PIN	F7	F7
DISC PIN DIA.	D5	D5
VALVE BODY O.D.	D1	D8
VALVE BODY WATERWAY DIA.	R7	R7
ADJACENT PIPING O.D.	R8	R8
ADJACENT PIPING I.D.	R9	R9
MAXIMUM PIPING BENDING MOMENT	M4	M4
NO. OF BODY BOLTS	N3	N3
DBC OF BODY BOLTS	X0	X0
ROOT AREA OF BODY BOLTS	A4	A4
LENGTH ACROSS GUSSETS	L	L
THICKNESS OF GUSSETS	T	T
DIA. OF FLANGE BOSSES	B	B
MODULUS OF ELASTICITY	E	E
	30,000,000	



## FDS - FLOW DYNAMIC SYSTEMS INTERNATIONAL INC.

## 12 CLASS 150 VALVE ASSEMBLY

CUSTOMER: NIAGARA WHAUK  
 SPEC. NO.: NHP2-P; 3040  
 REF. NO.: 19157  
 ITEM NO.: 4

## REFERENCE DWGS.

A.DSS 1 DWG. NO. 1112-301 REV.A  
 B.BODY DWG. NO. 1112-301 REV.A  
 C.DISC DWG. NO. 1112-301 REV.A  
 D.STEM DWG. NO. 1112-013 REV.A  
 E.PIN DWG. NO. 12600-069 REV.A  
 F.BRACKET DWG. NO. 8000-199 REV.-

## ALLOWABLE STRESSES (PSI)

A.BODY: 23400  
 B.STEM: 52800  
 C.PIN: 52800  
 D.DRILLING: 33700  
 E.BOLTING: 37500

DESIGN CONDITIONS  
 PRESSURE(PSIG)= 45  
 TEMPERATURE(F)= 340

## G LOADINGS

LEAD TORQUE= 3978  
 MEDIUM=AIR  
 FLOW DIRECTION=NONPREFERRED

TRANSVERSE= 3  
 VERTICAL= 4  
 LONGITUDINAL= 3

## DIMENSIONAL DATA

X1= 8.438	X2= 2.688	X3= 3.688	X4= 6	X5= 2.365	W1= 219	W2= 27
W4= .25	T1= .875	T2= 3	T3= 3.182	T4= 0	T9= .75	T0= .025
d3= 2.875	D1= 1.755	D1= 1.347	D= 11.703	E1= 1.625	E2= .938	
L2= .305	Y2= 1.557	N1= 4	A1= .1416	X6= 4.5	N2= 4	
A2= .1416	X7= 3.182	X8= 3.182	T5= 0.75	R5= 3	R6= 0	
%= 65	dp= .309	d1= 15	R7= 12.062	R8= 12.75	R9= 11.938	
L= 0	T= 0	B= 1	E= 30000000			

## NATURAL FREQUENCIES (HZ.)

LONGITUDINAL(Z) ACT./VALVE= 62 VS. 33HZ.  
 VERTICAL(Y) ACT./VALVE= 456 VS. 33HZ.  
 TRANSVERSE(X) ACT./VALVE= 70 VS. 33HZ.  
 LATERAL DISC/STEM= 906 VS. 33HZ.

## ACTUATOR BOLT STRESSES

SHEAR= 7786 PSI  
 TENSILE= 10397 PSI  
 COMBINED= 14795 PSI VS ALLOW.= 37500

BRACKET BOLT STRESSES  
 SHEAR= 8368 PSI  
 TENSILE= 17352 PSI  
 COMBINED= 21162 PSI VS ALLOW.= 37500

BRACKET STRESSES  
 SHEAR= 529 PSI  
 TENSILE= 3227 PSI  
 COMBINED= 3313 PSI VS ALLOW.= 18900

VALVE NECK STRESSES  
 SHEAR= 2976 PSI  
 TENSILE= 8782 PSI  
 COMBINED= 9340 PSI VS ALLOW.= 23400

STEM STRESSES  
 SHEAR= 10500 PSI  
 TENSILE= 4526 PSI  
 COMBINED= 13006 PSI VS ALLOW.= 52000

DISC PIN STRESS  
 SHEAR= 11997 PSI VS ALLOW.= 31380

SECTION MODULUS  
 VALVE= 192.79 IN43  
 PIPING= 47.09 IN43

ACTUATOR DEFLECTIONS  
 LONGITUDINAL= 7.0890000E-03 INCHES  
 VERTICAL= 1.7700000E-04 INCHES  
 TRANSVERSE= 3.8000000E-03 INCHES

## BODY BOLTING

NOT APPLICABLE

SIGNED... *[Signature]* ..... DATED... *1/17/87* .....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: N741C - SR8D - M3HW  
CUSTOMER: Niagara Mohawk  
P.O. NO.: NMPZ-P304 D-12177  
SPEC. NO.: NMPZ-P304 D # Add #1, #2, f #3  
REFERENCE NO.: 19157  
ITEM NO.: 4 AOU 109

REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-4</u>	REV. <u>A</u>
B. BODY DWG. NO.	<u>1113-301</u>	REV. <u>A</u>
C. DISC DWG. NO.	<u>2112-301</u>	REV. <u>A</u>
D. STEM DWG. NO.	<u>2510-013</u>	REV. <u>A</u>
E. PIN DWG. NO.	<u>7600-060</u>	REV. <u>A</u>
F. BRACKET DWG. NO.	<u>8000-199</u>	REV. <u>-</u>

ALLOWABLE STRESSES

A. BODY	<u>SA 351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA 514 GR C30 Carb H1075</u>	<u>52800</u>	PSI
C. PIN	<u>SACG4 GR 630 Cnd H1075</u>	<u>62500</u>	PSI
D. BRACKET	<u>CS</u>	<u>18500</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 3330 Case 4A IN-LBS  
MEDIA: Air  
FLOW DIRECTION: Preferred

G-LOADINGS

TRANSVERSE: 5  
VERTICAL: 4  
LONGITUDINAL: 3



SIZE 12" CLASS 150DIMENSIONAL DATAACTUATOR 4721C-3A80-M3.1L

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{2}$ VALVE	9,439	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{2}$ VALVE	2,689	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	3,699	X3
HEIGHT BRACKET	6	X4
HEIGHT VALVE NECK	2,665	X5
ACTUATOR WEIGHT	219	W1
BRACKET WEIGHT	27	W2
DISC WEIGHT	26	W4
THICKNESS OF BRACKET LOWER PLATE	.875	T1
WIDTH OF BRACKET	5	T2
WIDTH OF VALVE NECK	3.192	T3
THICKNESS OF VALVE NECK	0	T4
THICKNESS OF BRACKET SIDE PLATES	.75	T9
THICKNESS OF BRACKET TOP PLATE	1.625	T0
VALVE NECK O.D.	2.875	d3
PACKING BORE I.D.	1.255	D1
STEM DIA.	1.247	D1
GAGE DIA. OF DISC	1.703	D
WIDTH SMALL DIA. BACK OF DISC	1.625	E1
WIDTH LARGE DIA. OF DISC	.938	E2
FRUST WASHER THICKNESS	.305	L2
DIST. $\frac{1}{2}$ STEM TO FRONT OF DISC	1.557	Y2
NO. OF ACTUATOR BOLTS	4	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	.1416	A1
DBC OF ACTUATOR BOLTS	4.5	X6
NO. OF BRACKET/VALVE BOLTS	4	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	.1416	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	3.192	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	3.192	X8
LENGTH OF BRACKET	9.75	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	0	R5
DIA. OF VALVE BODY BOLT HOLES	0	R6
% TORQUE ON DISC PIN	.65	T7
DISC PIN DIA.	.309	d5
VALVE BODY O.D.	.170	d1
VALVE BODY WATERWAY DIA.	12.062	R7
ADJACENT PIPING O.D.	19.75	R8
ADJACENT PIPING I.D.	11.939	R9
MAXIMUM PIPING BENDING MOMENT	N/A	M4
NO. OF BODY BOLTS	4	N3
DBC OF BODY BOLTS	1	X0
ROOT AREA OF BODY BOLTS	0	A4
LENGTH ACROSS GUSSETS	0	L
THICKNESS OF GUSSETS	1	T
DIA. OF FLANGE BOSSES	30,000,000	B
MODULUS OF ELASTICITY		E



**POST-SEAL INTERNALS INC.**  
**NUCLEAR STRUCTURAL ANALYSIS**

**12 CLASS 150 VALVE ASSEMBLY**

PRINTED DOCUMENTATION

CUSTOMER: NIAGARA MOHAWK  
PROJECT NUMBER: 3040  
SPEC. NO.: NMP2-P; 3040  
REF. NO.: 19157  
DATE: 10/1/78

REFERENCE DUGS.

A.BODY DWG. NO. 1112-191 REV.A  
B. BODY DWG. NO. 1112-301 REV.A  
C.DISC DWG. NO. 2112-301 REV.A  
D. STEM DWG. NO. 2610-013 REV.A  
E.PIN DWG. NO. 12600-050 REV.A  
F.BRACKET DWG. NO. 2000-199 REV.-

ALLOWABLE STRESSES (PSI)

A.BODY: 23400  
B. STEM: 52900  
C. PIN: 52900  
D.BRACKET: 18900  
E.BOLTING: 37500

DESIGN CONDITIONS  
PRESSURE(PSIG)= 45  
TEMPERATURE(F)= 340

C LOADINGS

LOCK TORQUE= 3330  
MEDIA=AIR  
FLOW DIRECTION=PREFERRED

TRANSVERSE= 3  
VERTICAL= 4  
LONGITUDINAL= 3

DIMENSIONAL DATA

X1= 8.433	X2= 2.688	X3= 3.688	X4= 6	X5= 2.685	W1= 219	W2= 27
Y1= .25	Y2= .875	Y3= .5	Y4= 3.182	Y5= 0	Y6= .75	Y7= .815
d3= 2.875	D1= 1.755	D2= 1.247	D3= 11.703	E1= 1.625	E2= .938	
L2= .305	Y2= 1.557	N1= 4	A1= .1416	X6= 4.5	N2= 4	
A2= .1416	X7= 3.182	X8= 3.182	Z1= 7.75	R1= 0	R2= 0	
Z= .65	do= .309	di= 15	R2= 12.062	R3= 12.75	R9= 11.938	
L= 0	T= 0	B= 1	E= 30000000			

NATURAL FREQUENCIES (HZ.)  
LONGITUDINAL(Z) ACT./VALVE= 62 VS. 33HZ.  
VERTICAL(Y) ACT./VALVE= 48 VS. 33HZ.  
TRANSVERSE(X) ACT./VALVE= 70 VS.33HZ.  
LATERAL DISC/STEM= 906 VS.33HZ.

ACTUATOR BOLT STRESSES

SHEAR= 7273 PSI  
TENSILE= 10377 PSI  
COMBINED= 14376 PSI VS.ALLOW.= 37500

BRACKET BOLT STRESSES  
SHEAR= 7855 PSI  
TENSILE= 10552 PSI  
COMBINED= 20817 PSI VS.ALLOW= 37500

BRACKET STRESSES

SHEAR= 511 PSI  
TENSILE= 3097 PSI  
COMBINED= 3179 PSI VS.ALLOW= 18900

VALVE NECK STRESSES  
SHEAR= 2709 PSI  
TENSILE= 8782 PSI  
COMBINED= 11251 PSI VS.ALLOW= 23400

STEM STRESSES

SHEAR= 9746 PSI  
TENSILE= 4526 PSI  
COMBINED= 11297 PSI VS.ALLOW= 62900

DISC PIN STRESS  
SHEAR= 19139 PSI VS.ALLOW= 31830

SECTION MODULUS

VALVE= 171.79 IN<sup>4</sup>  
PIPING= 47.09 IN<sup>4</sup>

ACTUATOR DEFLECTIONS  
LONGITUDINAL= 7.08900000E-03 INCHES  
VERTICAL= 1.77000000E-04 INCHES  
TRANSVERSE= 5.80000000E-03 INCHES

BOLTY BOLTING

NOT APPLICABLE

SIGNED. *John G. Ferguson* ..... DATED... 10/18/78.....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: N761C - SR80 - M3HW  
CUSTOMER: Niagara Mohawk  
P.O. NO.: NMPZ-P304 D-12177  
SPEC. NO.: NMPZ-P304 D + 411 = 1.2 f + 3  
REFERENCE NO.: 19157  
ITEM NO.: 5 AOV105

REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-5</u>	REV. <u>C</u>
B. BODY DWG. NO.	<u>1112-301</u>	REV. <u>X</u>
C. DISC DWG. NO.	<u>2112-301</u>	REV. <u>A</u>
D. STEM DWG. NO.	<u>2510-013</u>	REV. <u>A</u>
E. PIN DWG. NO.	<u>7600-060</u>	REV. <u>A</u>
F. BRACKET DWG. NO.	<u>8000-199</u>	REV. <u>-</u>

ALLOWABLE STRESSES

A. BODY	<u>SA351 GR CF8M</u>	<u>23400</u>	PSI
B. STEM	<u>SA514 GR C10 Crf H1025</u>	<u>52800</u>	PSI
C. PIN	<u>SA514 GR 170 Crd H1025</u>	<u>52500</u>	PSI
D. BRACKET	<u>CS</u>	<u>18500</u>	PSI
E. BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 4485 Case 3B IN-LBS  
MEDIA: Air  
FLOW DIRECTION: Non-reversed

G-LOADINGS

TRANSVERSE: 3  
VERTICAL: 4  
LONGITUDINAL: 3



SIZE 12" CLASS 1C  
 DIMENSIONAL DATA  
 ACTUATOR N721C-SASO-A

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{2}$ VALVE	2.688	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{2}$ VALVE	8.438	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	3.688	X3
HEIGHT BRACKET	C	X4
HEIGHT VALVE NECK	2.005	X5
ACTUATOR WEIGHT	219	W1
BRACKET WEIGHT	37	W2
DISC WEIGHT	20	W4
THICKNESS OF BRACKET LOWER PLATE	.875	T1
WIDTH OF BRACKET	5	T2
WIDTH OF VALVE NECK	6.5	T3
THICKNESS OF VALVE NECK	2.939	T4
THICKNESS OF BRACKET SIDE PLATES	.75	T9
THICKNESS OF BRACKET TOP PLATE	.625	T0
VALVE NECK O.D.	0	G3
PACKING BORE I.D.	1.755	D1
STEM DIA.	1.247	D1
GAGE DIA. OF DISC	11.703	D
WIDTH SMALL DIA. BACK OF DISC	1.625	E1
WIDTH LARGE DIA. OF DISC	1.938	E2
THRUST WASHER THICKNESS	.305	L2
DIST. $\frac{1}{2}$ STEM TO FRONT OF DISC	1.577	Y2
NO. OF ACTUATOR BOLTS	4	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	.1416	A1
DBC OF ACTUATOR BOLTS	4.5	X6
NO. OF BRACKET/VALVE BOLTS	4	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	.1416	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	5	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	2	X8
LENGTH OF BRACKET	9.75	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	3.4	R5
DIA. OF VALVE BODY BOLT HOLES	1	R6
% TORQUE ON DISC PIN	65	T7
DISC PIN DIA.	.309	D5
VALVE BODY O.D.	16.0	D8
VALVE BODY WATERWAY DIA.	12.062	R7
ADJACENT PIPING O.D.	12.15	R8
ADJACENT PIPING I.D.	11.938	R9
MAXIMUM PIPING BENDING MOMENT	4/A	M4
NO. OF BODY BOLTS	1	N3
DBC OF BODY BOLTS	1	X0
ROOT AREA OF BODY BOLTS	1	A4
LENGTH ACROSS GUSSETS	0	L
THICKNESS OF GUSSETS	0	T
DIA. OF FLANGE BOSSES	0	B
MODULUS OF ELASTICITY	30,000,000	E



## FIGURE 1 - INTERNAL TORQUE, LOADS

## 12 CLASS 150 VALVE ASSEMBLY

CUSTOMER: NIAGARA MFG CO.  
 SPEC NO.: NMP2-P; 3040  
 REF. NO.: 19157  
 ITEM NO.:

## REFERENCE DWG'S.

A. BODY DWG. NO.: 1112-302 REV.A  
 C. DISC DWG. NO.: 2112-301 REV.A  
 D. STEM DWG. NO.: 2312-313 REV.A  
 E. PIN DWG. NO.: 12600-050 REV.A  
 F. BRACKET DWG. NO.: 8000-199 REV.-

## ALLOWABLE STRESSES (PSI)

A. SCUT: 35400  
 G. STEM: 62800  
 C. PIN: 62300  
 D. STEM: 18900  
 E. BOLTING: 37500

DESIGN CONDITIONS  
 PRESSURE (PSIG) = 45  
 TEMPERATURE (F) = 310

## G LOADINGS

LOCK TORQUE = 4185  
 MEDIA=AIR  
 FLOW DIRECTION=NONPREFERRED

TRANSVERSE = 3  
 VERTICAL = 4  
 LONGITUDINAL = 3

## DIMENSIONAL DATA

X1 = 2.688	X2 = 3.438	X3 = 3.388	X4 = 6	X5 = 2.665	W1 = 219	W2 = 27
T4 = .25	T2 = .375	T3 = .3	T4 = 2.735	T5 = .75		
d3 = 0	D1 = 1.755	D1 = 1.247	D = 11.703	E1 = 1.625	E2 = .933	
L2 = .305	Y3 = 1.557	N1 = 4	A1 = .1416	X6 = 4.5	N2 = 4	
Z2 = .4445	X7 = .5	X8 = .	T5 = 7.75	R3 = 3.4	R5 = .	
Z = .65	d5 = .309	d1 = 16	R7 = 12.062	R8 = 12.75	R9 = 11.938	
L = 0	T = 0	G = 0	E = 30000000			

NATURAL FREQUENCIES (HZ.)  
 LONGITUDINAL(Z) ACT./VALVE = 78 VS. 33HZ.  
 VERTICAL(Y) ACT./VALVE = 303 VS. 33HZ.  
 TRANSVERSE(X) ACT./VALVE = 123 VS. 33HZ.  
 LATERAL DISC/STEM = 906 VS. 33HZ.

## ACTUATOR BOLT STRESSES

SHEAR = 8162 PSI  
 TENSILE = 33719 PSI  
 COMBINED = 15107 PSI VS. ALLOW. = 37500

BRACKET BOLT STRESSES  
 SHEAR = 8337 PSI  
 TENSILE = 22749 PSI  
 COMBINED = 25495 PSI VS. ALLOW = 37500

## BRACKET STRESSES

SHEAR = 543 PSI  
 TENSILE = 3369 PSI  
 COMBINED = 3443 PSI VS. ALLOW = 18900

VALVE NECK STRESSES  
 SHEAR = 1380 PSI  
 TENSILE = 3578 PSI  
 COMBINED = 4278 PSI VS. ALLOW = 23400

STEM STRESSES  
 SHEAR = 11779 PSI  
 TENSILE = 4525 PSI  
 COMBINED = 14259 PSI VS. ALLOW = 62000

DISC PIN STRESS  
 SHEAR = 26773 PSI VS. ALLOW = 31680

SECTION MODULUS  
 VALVE = 270.23 IN<sup>3</sup>  
 PIPING = 47.09 IN<sup>3</sup>

ACTUATOR DEFLECTIONS  
 LONGITUDINAL = 4.4540000E-03 INCHES  
 VERTICAL = 1.1600000E-04 INCHES  
 TRANSVERSE = 1.9000000E-03 INCHES

BODY BOLTING  
 NOT APPLICABLE

SIGNED...*[Signature]*.....DATED...*[Date]*....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: N711C - SR80 - M3HW  
CUSTOMER: Ninzae Mahach  
P.O. NO.: NMPZ-P304D-12177  
SPEC. NO.: NMPZ-P304 D + Add o1, #2, f = 3  
REFERENCE NO.: 19157  
ITEM NO.: 5 A0VIII

REFERENCE DWGS.

A.	ASS'Y DWG. NO.	<u>19157-5</u>	REV.	<u>C</u>
B.	BODY DWG. NO.	<u>1113-301</u>	REV.	<u>A</u>
C.	DISC DWG. NO.	<u>2112-301</u>	REV.	<u>A</u>
D.	STEM DWG. NO.	<u>2510-013</u>	REV.	<u>A</u>
E.	PIN DWG. NO.	<u>7600-060</u>	REV.	<u>A</u>
F.	BRACKET DWG. NO.	<u>8000-199</u>	REV.	<u>-</u>

ALLOWABLE STRESSES

A.	BODY	<u>SA351 GR CF2M</u>	<u>23400</u>	PSI
B.	STEM	<u>SA514 GR 630 Cond H1075</u>	<u>52800</u>	PSI
C.	PIN	<u>SA514 GR 630 Cond H1075</u>	<u>52500</u>	PSI
D.	BRACKET	<u>CS</u>	<u>18500</u>	PSI
E.	BOLTING	<u>A193 GR B7</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 6776 CAG: 4B IN-LBS  
MEDIA: A1-  
FLOW DIRECTION: Preferred

G-LOADINGS

TRANSVERSE: 3  
VERTICAL: 7  
LONGITUDINAL: 3



SIZE 12 CLASS 12DIMENSIONAL DATAACTUATOR N721C-SK50-A

DESCRIPTION OF VARIABLE	INPUT NAME	COMPUTER NAME
TRANSVERSE DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	X1	X1
LONGITUDINAL DIST. ACTUATOR C.G. TO $\frac{1}{4}$ VALVE	X2	X2
VERTICAL DIST. ACTUATOR C.G. TO BRACKET	X3	X3
HEIGHT BRACKET	X4	X4
HEIGHT VALVE NECK	X5	X5
ACTUATOR WEIGHT	W1	W4
BRACKET WEIGHT	W2	W5
DISC WEIGHT	W4	W3
THICKNESS OF BRACKET LOWER PLATE	T1	T1
WIDTH OF BRACKET	T2	T2
WIDTH OF VALVE NECK	T3	T3
THICKNESS OF VALVE NECK	T4	T4
THICKNESS OF BRACKET SIDE PLATES	T9	T9
THICKNESS OF BRACKET TOP PLATE	T0	T0
VALVE NECK O.D.	d3	D3
PACKING BORE I.D.	Di	B5
STEM DIA.	D1	D1
GAGE DIA. OF DISC	D	D
WIDTH SMALL DIA. BACK OF DISC	E1	E1
WIDTH LARGE DIA. OF DISC	E2	E2
THRUST WASHER THICKNESS	L2	L2
DIST. $\frac{1}{4}$ STEM TO FRONT OF DISC	Y2	Y2
NO. OF ACTUATOR BOLTS	N1	N1
TENSILE STRESS AREA OF ACTUATOR BOLTS	A1	A1
DEC OF ACTUATOR BOLTS	X6	X6
NO. OF BRACKET/VALVE BOLTS	N2	N2
TENSILE STRESS AREA OF BRACKET/VALVE BOLTS	A2	A2
TRANSVERSE DIST. BETWEEN BRACKET BOLTS	X7	X7
LONGITUDINAL DIST. BETWEEN BRACKET BOLTS	X8	X8
LENGTH OF BRACKET	T5	T5
DISTANCE BETWEEN VALVE BODY BOLT HOLES	R5	R5
DIA. OF VALVE BODY BOLT HOLES	R6	R6
% TORQUE ON DISC PIN	%	F7
DISC PIN DIA.	d5	D5
VALVE BODY O.D.	d1	D8
VALVE BODY WATERWAY DIA.	R7	R7
ADJACENT PIPING O.D.	R8	R8
ADJACENT PIPING I.D.	R9	R9
MAXIMUM PIPING BENDING MOMENT	M4	M4
NO. OF BODY BOLTS	N3	N3
DEC OF BODY BOLTS	X0	X0
ROOT AREA OF BODY BOLTS	A4	A4
LENGTH ACROSS GUSSETS	L	L
THICKNESS OF GUSSETS	T	T
DIA. OF FLANGE BOSSES	B	B
MODULUS OF ELASTICITY	E	E
	30,000,000	



POST-SEAL INTERNATIONAL, INC.  
MICHIGAN DIVISION ANN ARBOR

12 CLASS 150 VALVE ASSEMBLY  
WITH 12" DIAMETER ACTUATOR

CUSTOMER: NIAGARA MOHAWK  
PROJ. NUMBER: 364671227  
SPEC. NO.: NMP2-P; 304D  
REF. NO.: 19157  
ITEM NO. 15

REFERENCE DWGS.

A. ASSEMBLY DWG. NO.: 11/157-5 REV.C  
B. BODY DWG. NO.: 1112-302 REV.A  
C. DISC DWG. NO.: 2112-301 REV.A  
D. STEM DWG. NO.: 2510-013 REV.A  
E. PIN DWG. NO.: 2500-060 REV.A  
F. BRACKET DWG. NO. 8000-199 REV.-

ALLOWABLE STRESSES (PSI)  
A. BODY: 23400  
B. STEM: 52300  
C. PIN: 52900  
D. BRACKET: 18700  
E. BOLTING: 37500

DESIGN CONDITIONS  
PRESSURE(PSIG)= 45  
TEMPERATURE= -340

LOCAL TORQUE= 3774  
MEDIA=AIR  
FLOW DIRECTION=PREFERRED

G LOADINGS  
TRANSVERSE= 3  
VERTICAL= 4  
LONGITUDINAL= 3

DIMENSIONAL DATA							
X1= 2.688	X2= 8.438	X3= 3.689	X4= 6	X5= 2.665	W1= 219	W2= 27	
Z4= .23	T1= .379	T2= 3	T3= 3.3	T4= 2.730	T5= .71	T6= .345	
d3= 0	D1= 1.755	D1= 1.247	D= 11.703	E1= 1.625	E2= .938		
L2= .305	Y2= 1.557	N1= 4	A1= .1416	X6= 4.5	N2= 4		
Z5= .413	X7= 3	X3= -	T5= 7.75	A2= 3.4	A3= -		
Z= .65	dp= .309	di= 16	R7= 12.062	R8= 12.75	R9= 11.938		
L= 0	T= 0	B= 0	E= 30000000				

NATURAL FREQUENCIES (HZ.)  
LONGITUDINAL(Z) ACT./VALVE= 78 VS. 33HZ.  
VERTICAL(Y) ACT./VALVE= 133 VS. 33HZ.  
TRANSVERSE(X) ACT./VALVE= 123 VS.33HZ.  
LATERAL DISC/STEM= 906 VS.33HZ.

ACTUATOR BOLT STRESSES  
SHEAR= 9935 PSI  
TENSILE= 19873 PSI  
COMBINED= 16632 PSI VS.ALLOW.= 37500

BRACKET BOLT STRESSES  
SHEAR= 9838 PSI  
TENSILE= 22749 PSI  
COMBINED= 26431 PSI VS.ALLOW= 37500

BRACKET STRESSES  
SHEAR= 605 PSI  
TENSILE= 38000 PSI  
COMBINED= 3903 PSI VS.ALLOW= 13900

VALVE NECK STRESSES  
SHEAR= 1640 PSI  
TENSILE= 2578 PSI  
COMBINED= 3374 PSI VS.ALLOW= 23400

STEM STRESSES  
SHEAR= 17796 PSI  
TENSILE= 4526 PSI  
COMBINED= 29203 PSI VS.ALLOW= 52000

DISC PIN STRESS  
SHEAR= 38943 PSI VS.ALLOW= 31500

SECTION MODULUS  
VALVE= 272.23 IN43  
PIPING= 47.09 IN43

ACTUATOR DEFLECTIONS  
LONGITUDINAL= 4.45400000E-03 INCHES  
VERTICAL= 1.16000000E-04 INCHES  
TRANSVERSE= 1.30000000E-03 INCHES

BODY BOLTING  
NOT APPLICABLE

SIGNED..... *John S. Johnson* ..DATED... 8/12/77....



NUCLEAR LOCA & SEISMIC ANALYSIS

VALVE SIZE: 12"  
VALVE CLASS: 150  
ACTUATOR: N7610 - SR80 - M3HW  
CUSTOMER: Niagara Mohawk  
P.O. NO.: NMPZ-P304 D-12177  
SPEC. NO.: NMPZ-P304 D & Add - L-2 f + 3  
REFERENCE NO.: 19157  
ITEM NO.: 5 A0VIII

REFERENCE DWGS.

A. ASS'Y DWG. NO.	<u>19157-5</u>	REV.	<u>C</u>
B. BODY DWG. NO.	<u>1112-301</u>	REV.	<u>A</u>
C. DISC DWG. NO.	<u>3112-101</u>	REV.	<u>A</u>
D. STEM DWG. NO.	<u>2510-013</u>	REV.	<u>A</u>
E. PIN DWG. NO.	<u>7600-060</u>	REV.	<u>A</u>
F. BRACKET DWG. NO.	<u>8000-199</u>	REV.	<u>-</u>

ALLOWABLE STRESSES

A. BODY	<u>SA351 GR CERPM</u>	<u>23400</u>	PSI
B. STEM	<u>SA514 GR C17 CAR H1075</u>	<u>52800</u>	PSI
C. PIN	<u>SA514 GR 670 CAR H1075</u>	<u>52500</u>	PSI
D. BRACKET	<u>CS</u>	<u>18900</u>	PSI
E. BOLTING	<u>A193 GR 137</u>	<u>37500</u>	PSI

DESIGN CONDITIONS

PRESSURE: 45 PSI  
TEMPERATURE: 340 DEG. F.

VALVE TORQUES

LOCA TORQUE: 4729 @ 70 CAR 4B IN-LBS  
MEDIA: A1-  
FLOW DIRECTION: Preferred

G-LOADINGS

TRANSVERSE: 3  
VERTICAL: 7  
LONGITUDINAL: 3



POST-SEAL INTERNATIONAL, INC.  
MODERN SEISMIC ANALYSIS

12 CLASS 150 VALVE ASSEMBLY  
SILVERWATER SPOT ACTUATOR

CUSTOMER: NIAGARA MONAUK  
PROJECT NO.: P3010-1111  
SPEC. NO.: NMP2-P;3040  
REF. NO.: 19157  
ITEM NO.: 1

REFERENCE DWGS.

A. ASSY DWG. NO. 19157 REV.C  
B. BODY DWG. NO. 1112-302 REV.A  
C. DISC DWG. NO. 2112-301 REV.A  
D. STEM DWG. NO. 1510-013 REV.A  
E. PIN DWG. NO. 12600-060 REV.A  
F. BRACKET DWG. NO. 8000-199 REV.-

ALLOWABLE STRESSES (PSI)

A. BODY: 23400  
B. STEM: 52800  
C. PIN: 52800  
D. BRACKET: 18900  
E. BOLTING: 37500

DESIGN CONDITIONS  
PRESSURE(PSIG)= 45  
TEMPERATURE, F= 340

G LOADINGS

TOCA TORQUE= 1729  
MEDIA=AIR  
FLOW DIRECTION=PREFERRED

TRANSVERSE= 3  
VERTICAL= 4  
LONGITUDINAL= 3

X1= 2.638	X2= 8.438	X3= 3.588	X4= 6	X5= 2.565	W1= 219	W2= 27
Y1= .25	T1= .375	T2= 3	T3= 3.5	T4= 3.738	T5= .75	T6= .25
G3= 0	O1= 1.755	D1= 1.247	D= 11.703	E1= 1.625	E2= .938	
L2= .305	Y2= 1.557	N1= 4	A1= .1416	X6= 4.5	N2= 4	
R2= .1418	X7= 3	X8= 2	T5= 7.75	R5= 3.7	R6= 1	
Z= .65	dp= .309	d1= 16	R7= 12.062	R8= 12.75	R9= 11.938	
L= 0	T= 0	B= 0	E= 30000000			

NATURAL FREQUENCIES (HZ.)

LONGITUDINAL(Z) ACT./VALVE= 78 VS. 33HZ.  
VERTICAL, ACT./VALVE= 58 VS. 33HZ.  
TRANSVERSE(X) ACT./VALVE= 123 VS.33HZ.  
LATERAL DISC/STEM= 906 VS.33HZ.

ACTUATOR BOLT STRESSES

SHEAR= 8350 PSI  
TENSILE= 1057 PSI  
COMBINED= 15265 PSI VS.ALLOW.= 37500

BRACKET BOLT STRESSES

SHEAR= 3497 PSI  
TENSILE= 20737 PSI  
COMBINED= 25590 PSI VS.ALLOW= 37500

BRACKET STRESSES

SHEAR= 549 PSI  
TENSILE= 3104 PSI  
COMBINED= 3492 PSI VS.ALLOW= 18900

VALVE NECK STRESSES

SHEAR= 1408 PSI  
TENSILE= 2578 PSI  
COMBINED= 3199 PSI VS.ALLOW= 31400

STEM STRESSES

SHEAR= 12420 PSI  
TENSILE= 4523 PSI  
COMBINED= 14000 PSI VS.ALLOW= 55000

DISC PIN STRESS

SHEAR= 27179 PSI VS.ALLOW= 31480

SECTION MODULUS

VALVE= 272.03 IN<sup>3</sup>  
PIPING= 47.09 IN<sup>3</sup>

ACTUATOR DEFLECTIONS

LONGITUDINAL= 4.4540000E-03 INCHES  
VERTICAL= 1.1600000E-04 INCHES  
TRANSVERSE= 1.3000000E-03 INCHES

NOT APPLICABLE

SCREW BOLTING

SIGNED....*[Signature]*.....DATED..5/14/84.....



APPENDIX H

Miscellaneous Calculations



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title D. I. piping - flow AP with valve, Z = 70° Page H-1  
Calc. By J. P. Murphy 7/16/84 Checked By \_\_\_\_\_

12" valve  $\theta 70^\circ$

$$P_1 = 15.7 \text{ psia}$$

$$Q = 1300 \text{ SCFM} = 28000 \text{ SCFH}$$

$$G = 1 \quad Z = 1 \quad T = 150^\circ\text{F}$$

$$C_v @ 70^\circ = 3113 \quad X_t @ 70^\circ = .42 \quad F_k = 1$$

VALVE SIZE = 12 IN. CLASS = 150

~~Q = 78000~~ ~~Cv = 3113~~ ~~P1 = 15.7~~ ~~Fp = 1~~  
~~Fk = 1~~ ~~Xt = .42~~ ~~G = 1~~ ~~'F = 150~~ ~~Z = 1~~

~~DELTA P = 0.0152 PSI~~

$\theta 90^\circ$

$$C_v @ 90^\circ = 4942 \quad X_t @ 90^\circ = .33$$

VALVE SIZE = 12 IN. CLASS = 150

~~Q = 78000~~ ~~Cv = 4942~~ ~~P1 = 15.7~~ ~~Fp = 1~~  
~~Fk = 1~~ ~~Xt = .33~~ ~~G = 1~~ ~~'F = 150~~ ~~Z = 1~~

~~DELTA P = 0.0052 PSI~~



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title \_\_\_\_\_ Page H-2  
Calc. By J. Culpeper 7/16/84 Checked By \_\_\_\_\_

14" VALVE @ 70°

$$P_1 = 15.7 \text{ psia}$$

$$Q = 2200 \text{ SCFM} = 132000 \text{ SCFH}$$

$$G = 1 \quad Z = 1 \quad T = 150^{\circ}\text{F}$$

$$C_v @ 70^{\circ} = 3979 \quad X_T @ 70 = .42 \quad F_k = 1$$

VALVE SIZE = 14 IN. CLASS = 150

Q = 132000	Cv = 3979	P1 = 15.7	Fp = 1
Fk = 1	Xt = .42	G = 1	'F = 150
Z = 1			

DELTA P = 0.0232 PSI

@ 90°

$$C_v @ 90^{\circ} = 6317 \quad X_T = .33$$

VALVE SIZE = 14 IN. CLASS = 150

Q = 132000	Cv = 6317	P1 = 15.7	Fp = 1
Fk = 1	Xt = .33	G = 1	'F = 150
Z = 1			

DELTA P = 0.0091 PSI



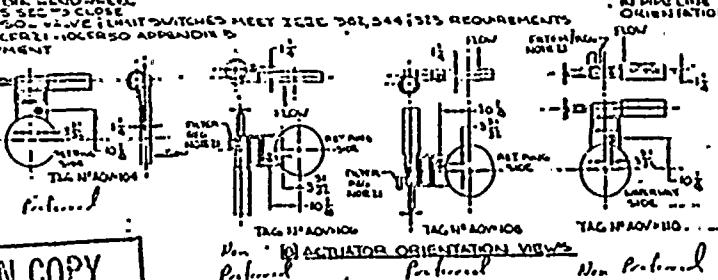




ACTUATOR INFORMATION

1) BETTS N712C-5100-M5HW WITH 1" BORE, 1/4" NPT-76 DA KEYWAY, FOR SWAY  
2) ASCO SWAY SOL. INPKC031041, 120 VAC  
3) ISOLATED SWITCHES NAMCO EA-745-50100 IN OPEN POS (CLOSE POS)  
4) FUSIBLE REGULATOR 1A715 12-150V SET AT 80PSIG  
5) INTERNAL PRESSURE-1# DIA. SWING VALVE  
6) CYCLE TIME: 5 SEC TO OPEN & 5 SEC TO CLOSE  
7) ISOLATED TO LEAD TIME 5 SEC  
8) LIMIT SWITCHES MEET IECIE 762, 344-325 REQUIREMENTS  
9) THE REQUIREMENTS OF ISOFERREL NOVOSO APPENDIX B  
10) EQUIVALENT TO CLASS III EQUIPMENT  
11) BETTS DIA 1# SP313

1) MATERIAL NO.  
M51-5  
2) VALVE TAG NO.  
E205-A0V  
3) ACTUATOR TAG LAYOUT



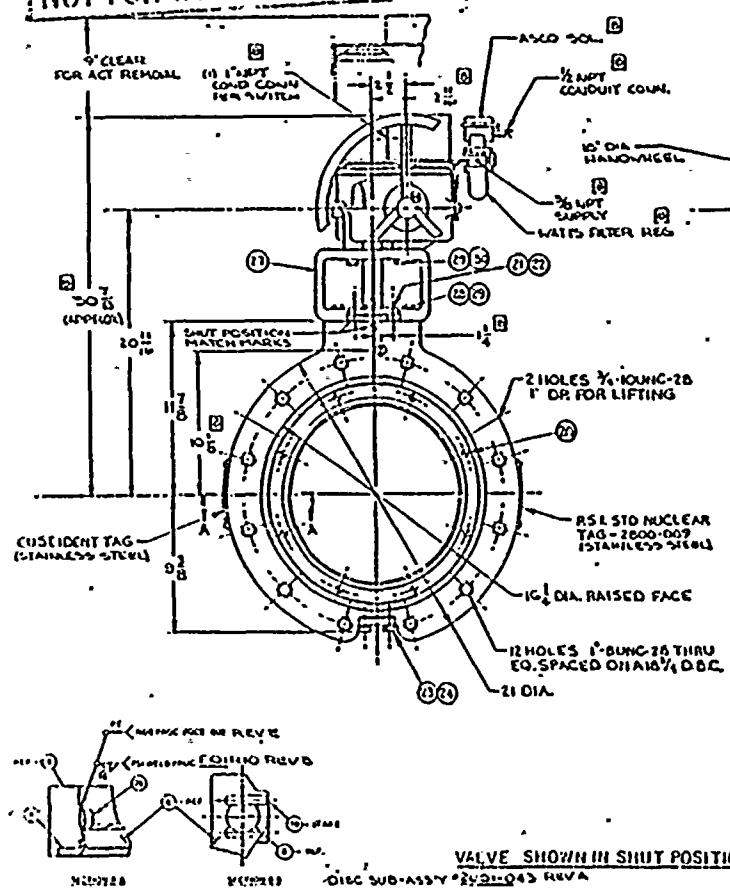
SHELL MOTEUR (SOM)

1) MAKE BODY FROM 1114-SOL AL  
2) MAKE DISC FROM 2114-SOL AL REVD SEE NOTE C1015  
3) MAKE MOUNTING BRACKET FROM 0000-AL OR REV  
4) FILTER FINE MUST BE INLET AT ASSY. TO REMAIN IN  
UPRIGHT POSITION WHEN ACT. VALVE ASSY IS MOUNTED  
IN PIPE LINE TO CONFIGURATION SHOWN IN ACTUATOR  
ORIENTATION VIEW

POSITION	VALVE
OPEN	1114-AL
CLOSE	2114-AL
DESIGN TEMP: 120°F	
YEAR OF MFR: 1985	
VALVE TAG NO.: E205-A0V	
VALVE DESCRIPTION NO.	
NATIONAL BOARD NO.	

CUST IDENT TAG LAYOUT

INFORMATION COPY  
NOT FOR MANUFACTURE





## ACTUATOR INFORMATION

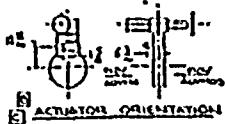
III. NITRIC ACID VALVE WITH 1" BORE 1/4" NPT 70 DP KEYWAY  
SWIVEL SOL VALVE NPCKC2316SL, 120VAC

1. LIMIT SWITCHES HAMCO 8A-TCD-8000 (OPEN POS. IN CLOSE POS)  
HAMCO EL-OIO-2337 LEVER  
WATTS 211-03G SET TO 20 PSIG  
HAMCO CUSHIONER 10 DIA. HANDWHEEL  
SWIVEL VALVE TO OPEN & SWL TO CLOSE  
WMA TO CERTIFY THAT SOL. VALVE & LIMIT SWITCHES MEET TECS  
2041-225 REQUIREMENTS. THE REQUIREMENTS OF WMA  
INFERNO APPENDIX B APPLY TO CLASS 1E EQUIPMENT

BETIS CERE ACT DNG = SP 9313

FEA SERIAL NR.  
PIST-5  
VALVE TAG NR.  
2CPS-AVII

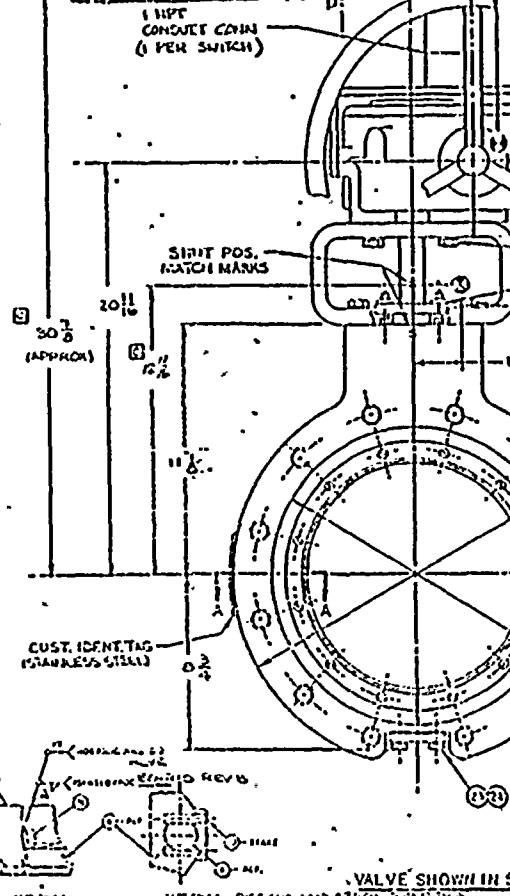
## ACTUATOR, TAG LAYOUT



- GEN. NOTES (CONT'D)  
10. MAKE DISC FROM 1112-SOL-C4 REV B NOTE C.10.113  
11. MAKE BODY FROM 1112-SOL-ASL  
12. MAKE MOUNTING BRACKET 10000-11 BL REV-

POSITIONAL  
12" CLOSPD 120  
VALVE DESCRIPTION NO.  
WVF 05-A-120  
VALVE MATERIAL 16SS PSI  
DISCH. SCALES 11117.2  
DISCH. PRESS. 110 PSIG  
DISCH. TEMP. 70°F  
YEAR OF MFR: 1983  
VALVE TAG NO. 700-120V  
NATIONAL BOARD NO.  
C101 LOCTITE TAG LAYOUT

9 DIA FOR ACT  
HANCO  
NOT FOR MANUFACTURE



ACTUATOR ORIENTATION

## C101 LOCTITE TAG LAYOUT

MANUFACTURER 1000-11  
ACTUATOR 1000-11  
PART NO. 11117.2  
REV. C

- GENERAL NOTES  
1. ALL STAMPING, BODY AND DISC SHALL BE IN ACCORDANCE WITH PGS 116, DRAWING NO. 1100-010 HEAVY.  
2. SPECIFIC PROCESS REQUIREMENTS  
3. DESIGN PLATE PERFORMS AS PICTURED IN DRAWING  
4. HEAT TREAT PER FORM NO. PGS-100, REV. D  
5. PURCHASED ITEMS ARE TO BE INSPECTED IN ACCORDANCE WITH THE PURCHASE AGREEMENT AND PURCHASE CONTRACT  
6. SPECIAL INSPECTION IS TO BE MADE BY THE SAME AS THE DISC AND DISC SHALL BE RECHECKED IN ACCORDANCE WITH PGS-100  
7. A CERTIFICATE OF COMPLIANCE TO THE MATERIAL SPECIFICATION IS REQUIRED.  
8. RADIONUCLIDES TEST PER ASME B & PV CODE SECTION 3-1973  
9. RADIONUCLIDES TEST PER ASME B & PV CODE SECTION 3-1973  
10. LIQUID PENETRANT TEST PER ASME B & PV CODE SECTION 3-1973  
11. MAGNETIC PARTICLE TEST PER ASME B & PV CODE SECTION 3-1973  
12. VALVE ASSEMBLY DESIGN IS TO BE ATTACHED TO VALVE WITH THE SAME SURFACES AS  
SECTION 3-1973 WHICH INCLUDES THE CALIBRATION IN ASME B & PV CODE SECTION 3-1973

## CUSTOMER NIAGARA MOHAWK POWER CORPORATION

CUSTOMER NO. NMP2-P504D/1177

- ⑥ TOTAL ASSEMBLY 101 LBS. ACT/BRKT WT 1216 LBS. VALVE WT 1151 LBS  
VALVE NO. 4942 (10" OPEN)  
CENTER OF GRAVITY: ⑦ TOTAL ASSY ⑧ ACTUATOR  
VALVE VALVE WEIGHT 1400-001 (WITH THE FOLLOWING: 2 CPS-AVII  
(NOTE: 11117.2 TO BE ATTACHED TO VALVE WITH THE SAME SURFACES AS  
2 CPS-AVII))  
⑨ AUSTENITIC STAINLESS STEEL CASTINGS TO CONTAIN 3% MAX FERRITE AS  
DETERMINED BY ANALYSIS.  
⑩ REMOVE PACKING AFTER ALL TESTING IS COMPLETED AND REPLACE  
PACKING GLAND AND FOLLOWER AND HANDTIGHTEN NUTS. SECOND SET  
OF TACKING TO BE ATTACHED TO VALVE IN PLASTIC BAG.  
⑪ TORQUE NUTS TO 65-70IN. LBS (WHEN SECOND SET OF PACKING IS  
INSTALLED BY CUSTOMER).  
⑫ FINISHED TEEFLITE SEALS SHALL BE BOILED IN DEMINERALIZED WATER  
FOR A MINIMUM OF 24 HOURS PRIOR TO ASSEMBLY.  
⑬ VALVE BODY AND GASKET RETAINER SHELL BE PAINTED AFTER  
HYDROSTATIC TESTS.

NH2 MILE POINT NUC. STATION - UNIT 2  
NIAGARA MOHAWK POWER CORPORATION  
J.O. NO. NITI, P.O. NO. NAP2-P504D

ITEM	DESCRIPTION	QUANTITY		
		DESCRIPTION	QTY	REVISION
1	DISC	1	11117.2	A
2	SWIVEL VALVE	1	11117.2	A
3	SWIVEL VALVE	1	11117.2	A
4	SWIVEL VALVE	1	11117.2	A
5	SWIVEL VALVE	1	11117.2	A
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189	SWIVEL VALVE	1	11117.2	A
190	SWIVEL VALVE	1	11117.2	A
191	SWIVEL VALVE	1	11117.2	A
192	SWIVEL VALVE	1	11117.2	A
193	SWIVEL VALVE	1	11117.2	A</



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**POSI-SEAL**  
INTERNATIONAL, INC.

**TECHNICAL BULLETIN NO. 2**  
**VALVE SIZING**

**JUNE 82**

## I. INTRODUCTION

This technical bulletin is intended to assist in the selection of Posi-Seal trunnion valves to control a given set of flow conditions.

## II. FLOW COEFFICIENT - $C_v$

The flow coefficient or  $C_v$  of a valve is used to describe its inherent flow capacity. This value is defined as the number of U.S. gallons of water per minute at standard conditions (60°F and 14.7PSIA) that will flow thru a valve at a constant 1.0PSI pressure drop. Accordingly, a  $C_v$  value based on extensive flow testing of valves at these conditions has been assigned to each Posi-Seal trunnion valve. Using this  $C_v$  value, the capacity of each valve with regard to other fluids under various conditions can be related to this basic  $C_v$  value.

## III. VALVE SIZING AND SELECTION

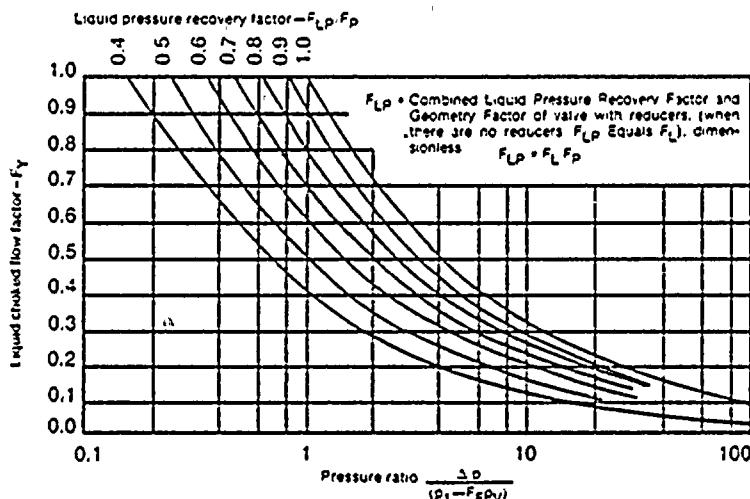
Proper valve sizing and selection of Posi-Seal trunnion valves are to be based on the following criteria.

1. Throttling control valves should be sized between the 15° and 80° disc open position.

2. To prevent actuator/valve instability resulting from a hydrodynamic torque reversal when flowing liquids for throttling service, valves should be installed with the retaining ring side of the valve downstream. Complete information on this torque reversal phenomenon can be found in Posi-Seal Technical Bulletin No. 1A.
3. The maximum recommended operating differential pressures and pipeline velocities noted in Posi-Seal Technical Bulletin No. 6 are to be used in valve selection.
4. Valve materials of construction are governed by media and operating conditions.
5. Liquid, gas and steam gas flow limitations are governed by the parameters noted in this technical bulletin.



FIGURE 1



## PIPING EFFECTS

For valves that are installed in piping where the connecting pipe diameter is greater or less than the nominal valve diameter, the factor  $F_p$  is utilized in the sizing equations to account for additional friction losses due to piping reducers or expanders directly adjacent to the valve.

WHERE:

$$F_p = \sqrt{\frac{C_{vp}^2}{C_v^2 - C_{vp}^2}}$$

$$C_{vp} = \frac{29.8D^2}{\sqrt{\left(1 - \frac{D^2}{D_{21}^2}\right)^2 + .5\left(1 - \frac{D^2}{D_{12}^2}\right)}}$$

$C_{vp}$  = flow coefficient of pipe enlargement and contraction combined.

$C_v$  = valve flow coefficient

$D$  = ID of pipe equal to valve size, inches

$D_1$  = ID of upstream pipe, inches

$D_2$  = ID of downstream pipe, inches

FOR INSTALLATIONS WHERE  $D_1$  EQUALS  $D_2$ :

WHERE:

$$C_{vp} = KD^2 \quad D = ID \text{ of pipe equal to valve size, inches}$$

$K$  = Refer to Fig. 2

FIGURE 2

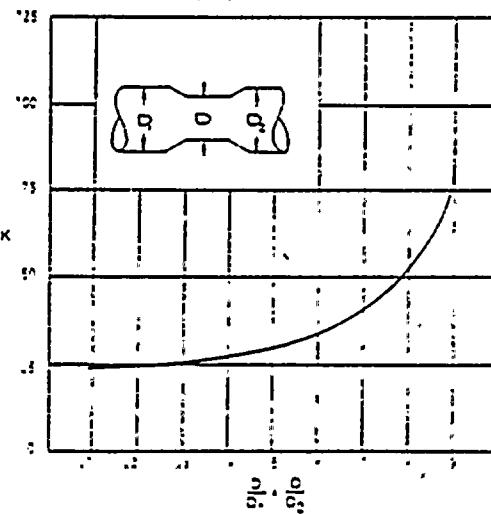




FIGURE 4

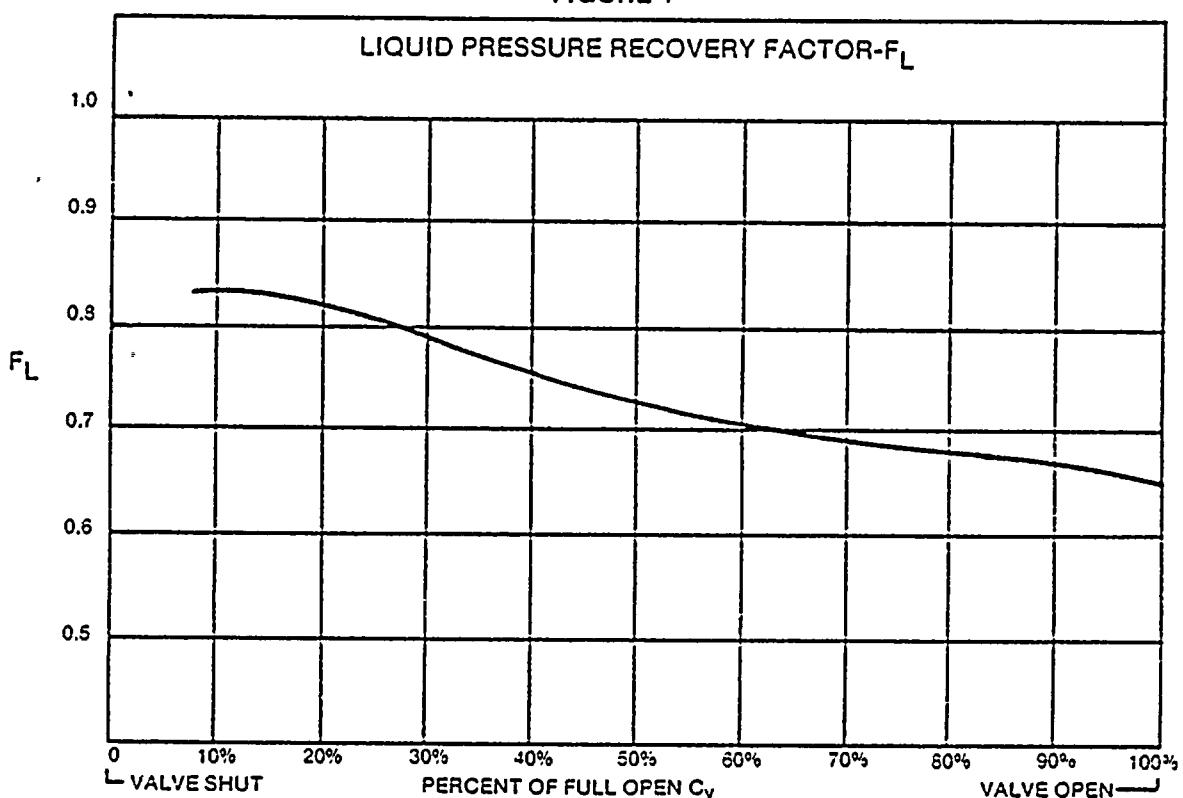
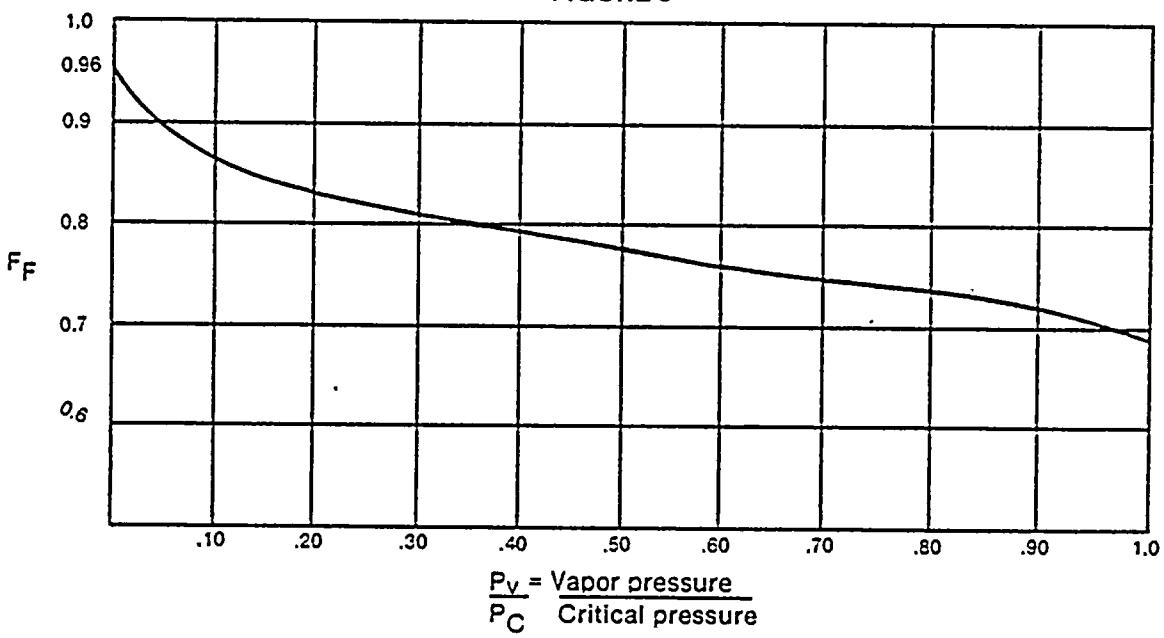


FIGURE 5





## CRITICAL FLOW

$$Q_{MAX} = 907.12 F_p C_v P_1 \sqrt{\frac{F_K X_T}{G T_1 Z}}$$

OR

$$C_v \text{ MIN} = \frac{Q}{907.12 F_p P_1 \sqrt{\frac{F_K X_T}{G T_1 Z}}}$$

$$\Delta P_c = F_K X_T P_1$$

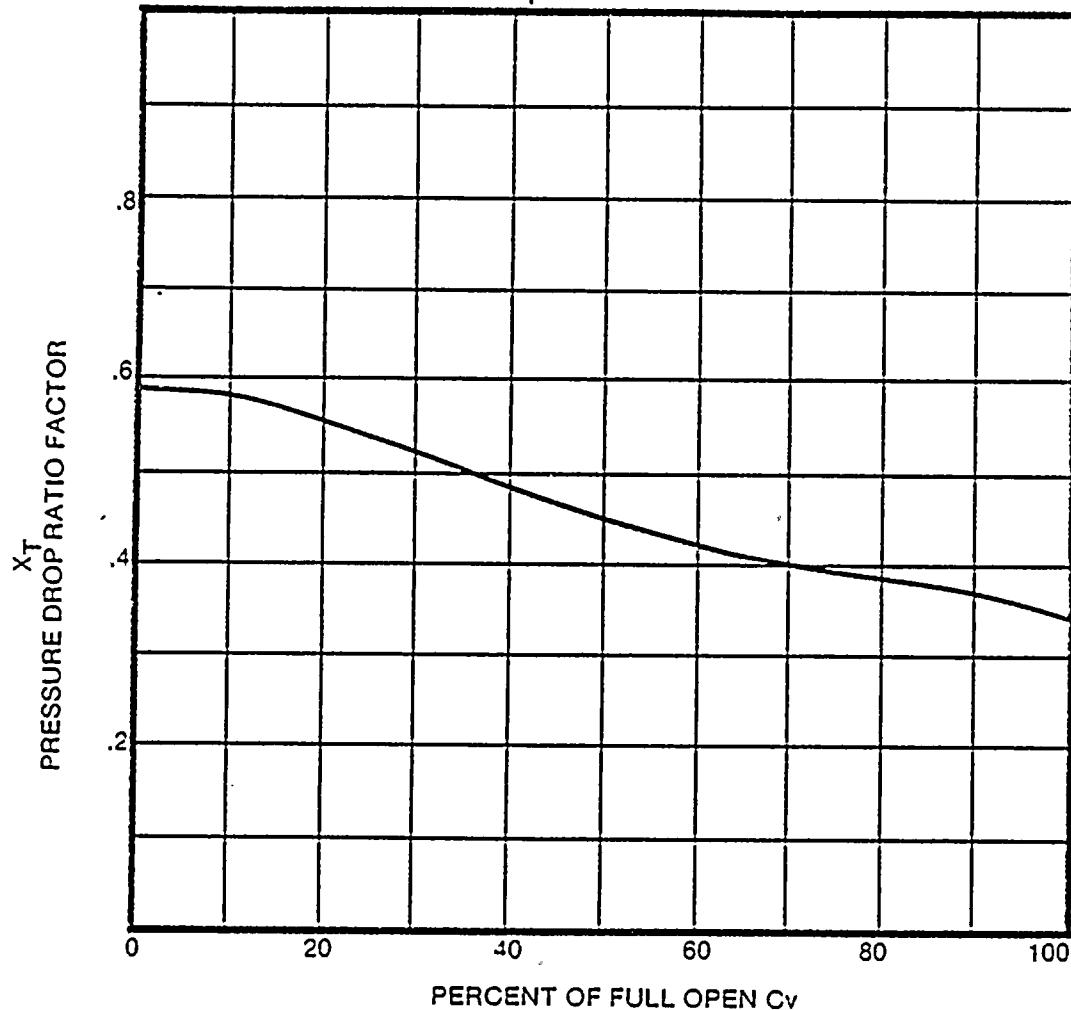
$Q_{MAX}$  = Max Flow that can pass through valve at the stated conditions.

$C_v \text{ MIN}$  = Minimum Required  $C_v$  in order to pass flow at the stated conditions.

$\Delta P_c$  = Max usable differential pressure drop above which no increase in flow will occur.

$F_L$  = Rated Liquid Pressure Recovery Factor (See Figure 4).

FIGURE 6  
 $X_T$  VS. % FLOW





# Posi-Seal Technical Bulletin No. 2

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TABLE 1

FLUID	FORMULA OR SYMBOL	MOLECULAR WEIGHT	BOILING POINT °F (°C)	VAPOR PRESSURE °OF PSIA <sup>1</sup>	CRITICAL TEMPERATURE °F	CRITICAL PRESSURE PSIA <sup>2</sup>	SPECIFIC GRAVITY	
							140°F/60°F	MS. G. 140°F/60°F AIR <sup>3</sup>
Acetic Acid	$\text{HC}_2\text{H}_5\text{O}_2$	60.05	245		611	241	1.05	
Acetic Anhydride	$\text{C}_2\text{H}_3\text{CO}_2\text{O}$	102.09	283			270		1.28
Acetone	$\text{C}_3\text{H}_6\text{O}$	58.08	153		455	631	0.79	1.11
Acetylene	$\text{C}_2\text{H}_2$	26.02	-119		37	911	0.62	1.01
Air	$\text{N}_2\text{O}_2$	28.97	-31°		221	54°	1.06	1.0
Alcohol, Ethyl	$\text{C}_2\text{H}_5\text{O}$	46.07	173	2.3°	270	225	0.794	1.39
Alcohol, Methyl	$\text{CH}_3\text{O}$	32.04	148	1.63°	162	1174	0.786	1.11
Ammonia	$\text{NH}_3$	17.03	-35	0.1°	270	1636	0.62	0.82
Aniline	$\text{C}_6\text{H}_5\text{N}$	93.12	563		738	770	1.02	
Argon	$\text{Ar}$	39.91	-302		198	713	1.16	1.38
Benzene	$\text{C}_6\text{H}_6$	78.11	178	3.00°	552	711	0.88	1.69
Bromine	$\text{Br}_2$	159.84	138		573	1485	0.75	0.88
Butadiene	$\text{CH}_2=\text{CH}-\text{CH}=\text{CH}_2$	54.09	24			617	0.63	
n-Butane	$\text{C}_4\text{H}_{10}$	58.12	51	51.6°	303	350	0.58	1.0
Butyl Alcohol	$\text{C}_4\text{H}_9\text{OH}$	74.12	212			711		1.61
Carbon Dioxide	$\text{CO}_2$	44.01	-109	830		110	0.57	1.52
Carbon Monoxide	$\text{CO}$	28.01	514		423	507	0.82	1.07
Carbon Tetrachloride	$\text{CCl}_4$	156.84	17		342	501	0.83	0.81
Chlorine	$\text{Cl}_2$	70.94	-73°	55	211	1118	1.12	1.15
Dowtherm A						132	1.05°	
Ethane	$\text{C}_2\text{H}_6$	30.07	-227			385	1.07°	1.72
Ethyl Chloride	$\text{C}_2\text{H}_5\text{Cl}$	54.52	55			2730	0.7	2.02
Ethylene	$\text{C}_2\text{H}_4$	28.05	-131		48	710	0.77	1.07
Ethyl Ether	$\text{C}_2\text{H}_5\text{O}_2$				133	522	1.46	
Fluorine	$\text{F}_2$	38.01	-53°	2.0°	1.3°	109	0.71	1.31
Helium	$\text{He}$	4.003	-454		150	35	0.18	0.11
Hydrochloric Acid	HCl	36.47	-115		130	133	0.91	
Hydrogen	$\text{H}_2$	2.016	-422		130	133	0.07	
Hydrogen Chloride	HCl	36.47	-117	0.7°	133	1138	0.86	1.26
Hydrogen Sulfide	$\text{H}_2\text{S}$	34.07	-76	252	115	1338	0.71	1.17
Isobutane	$\text{C}_4\text{H}_{10}$	58.11	11	72.2	274	529	0.56	0.91
Isopropyl Alcohol	$\text{C}_3\text{H}_8\text{O}$	60.09	104		155	779	0.78	0.98
Methane	$\text{CH}_4$	16.04	-253		110	673	0.50	0.55
Methyl Chloride	$\text{CH}_3\text{Cl}$	58.19	-57	2.0°	207	140	0.74	
Naphthalene	$\text{C}_{10}\text{H}_8$	128.16	221				1.12	1.15
Nitric Acid	$\text{HNO}_3$	63.02	187				1.5	
Nitrogen	$\text{N}_2$	28.01	-320	0.52°	433	103	1.31	1.07
n-Octane	$\text{C}_8\text{H}_{18}$	114.23	258		361	361	0.71	0.91
Oxygen	$\text{O}_2$	32.00	-297		131	730	1.14	1.103
n-Pentane	$\text{C}_5\text{H}_{12}$	72.11	-26	1.5°	386	183	0.63	1.49
Phenol	$\text{C}_6\text{H}_5\text{OH}$	94.11	558		786	889	1.07	
Phosphoric Acid	$\text{H}_3\text{PO}_4$	98.00	415				1.65	
Propane	$\text{C}_3\text{H}_8$	44.10	-47	130°	206	617	0.51	1.52
Propylene	$\text{CH}_2=\text{CH}-\text{CH}_3$	42.08	-54		198	661	0.61	0.61
Propyl Alcohol	$\text{CH}_3\text{CH}_2\text{CH}_2\text{OH}$	60.09	208			735		0.80
Propyl Chloride	$\text{CH}_3\text{CH}_2\text{CH}_2\text{Cl}$	78.54	115			663		0.89
Refrigerant 11	$\text{CCl}_2\text{F}$	157.58	75	13.1	398	635		0.94
Refrigerant 12	$\text{CCl}_2\text{F}_2$	120.93	-22	7.2	234	597		4.2
Refrigerant 21	$\text{CHCl}_2\text{F}$	102.93	45	3.1	353	750		3.82
Refrigerant 22	$\text{CHClF}_2$	96.48	-41	121.5	205	715		
Styrene	$\text{C}_8\text{H}_8$	104.15	295	4.21°	766	580	0.71	0.59
Sulfur Dioxide	$\text{SO}_2$	63.0	14	53.1	316	1142	1.39	1.21
Toluene	$\text{C}_7\text{H}_8$	92.14	231	1.07°	605	611	0.87	0.13
Water	$\text{H}_2\text{O}$	18.016	212	0.95	76	5296.2	1.00	0.02

1. Vapor Pressure in PSIA at 100°F

2. Specific Gravity at 49.3°F.

3. Specific Gravity at 350.4°F.



TABLE 3  
COMPRESSIBILITY FACTORS FOR GAS

Gas	Pressure						
	atm	psia	-100 F	0 F	200 F	1000 F	2000 F
Argon	1	14.7	0.997	0.999	1.000	1.000	1.000
	10	147	0.970	0.987	0.999	1.003	1.002
	40	588	0.877	0.952	0.995	1.011	1.009
	100	1470	0.690	0.887	0.995	1.029	1.022
Carbon monoxide	1	14.7	0.997	0.999	1.000	1.000	1.000
	10	147	0.973	0.991	1.001	1.004	1.003
	40	588		0.967	1.007	1.017	1.012
	100	1470			1.027	1.044	1.031
Carbon dioxide	1	14.7		0.991	0.997	1.000	1.000
	10	147		0.910	0.974	1.001	1.003
	40	588			0.894	1.006	1.010
	100	1470			0.721	1.018	1.026
Hydrogen	1	14.7	1.001	1.001	1.001		
	10	147	1.007	1.006	1.005		
	40	588	1.028	1.026	1.021		
	100	1470	1.076	1.067	1.052		

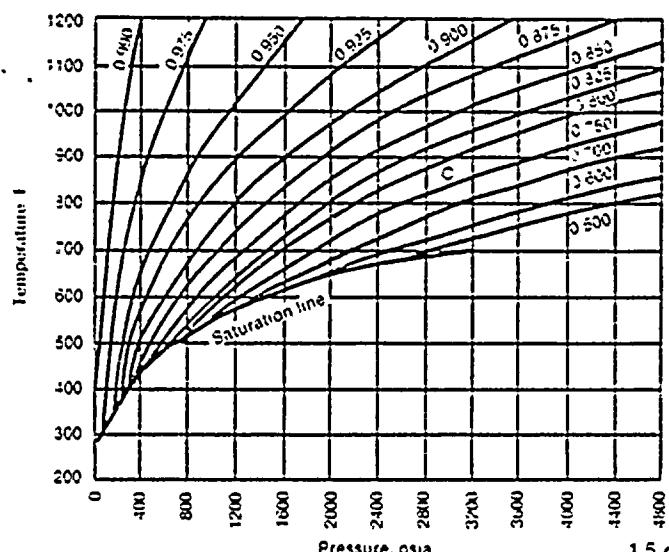
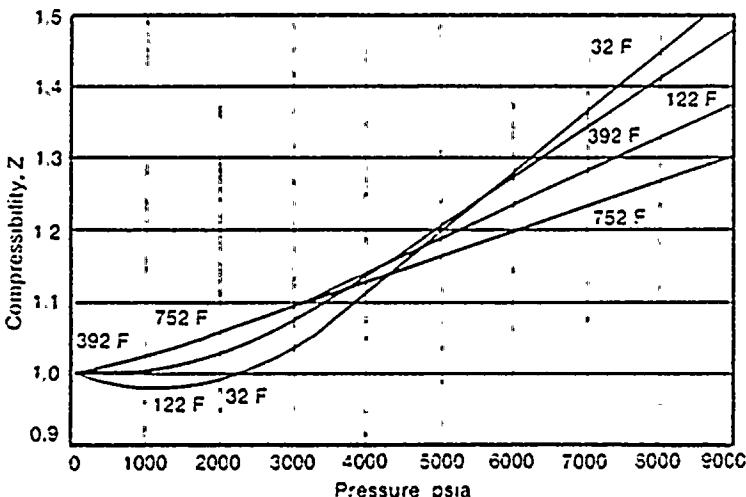


FIGURE 10  
COMPRESSIBILITY FACTORS  
FOR SUPERHEATED STEAM

FIGURE 11  
COMPRESSIBILITY FACTORS  
FOR NITROGEN →





**TABLE 6**  
**SUPERHEATED VAPOR**

Pressure (psia)	Temperature (°F)														
	200	260	300	360	400	460	500	600	700	800	900	1000	1100	1200	
10	v	38.85	42.56	45.00	48.63	51.04	54.05	57.05	63.04	69.01	74.98	80.95	86.92	92.88	96.84
	h	1146.6	1175.1	1193.9	1221.9	1240.6	1268.7	1287.5	1335.1	1383.4	1432.5	1482.4	1533.2	1585.0	1637.6
	s	1.7927	1.6341	1.8595	1.8950	1.9172	1.9488	1.9689	2.0160	2.0595	2.1002	2.1383	2.1744	2.2096	2.2413
20	v		21.11	22.36	24.21	25.43	27.25	28.46	31.47	34.47	37.46	40.45	43.44	46.42	49.41
	h		1172.2	1191.6	1220.3	1239.2	1267.6	1286.6	1334.4	1382.9	1432.1	1482.1	1533.0	1584.7	1637.4
	s		1.7545	1.7808	1.8170	1.8396	1.8716	1.8918	1.9392	1.9829	2.0235	2.0618	2.0978	2.1321	2.1648
50	v		8.773	9.557	10.065	10.815	11.339	12.532	13.744	14.950	16.152	17.352	18.550	19.747	
	h		1184.3	1215.2	1235.1	1264.5	1283.9	1332.5	1381.4	1430.9	1481.1	1532.1	1584.0	1636.8	
	s		1.6721	1.7112	1.7349	1.7680	1.7687	1.8368	1.8809	1.9219	1.9602	1.9964	2.0308	2.0636	
100	v		4.663	4.937	5.333	5.589	6.218	6.835	7.446	8.052	8.656	9.259	9.860		
	h		1205.7	1227.6	1258.8	1279.1	1329.1	1378.9	1428.9	1479.5	1530.8	1582.9	1635.7		
	s		1.6258	1.6518	1.6869	1.7085	1.7581	1.8029	1.8443	1.8829	1.9193	1.9538	1.9867		
150	v		3.023	3.223	3.502	3.081	4.113	4.532	4.944	5.352	5.758	6.162	6.564		
	h		1195.1	1219.4	1252.9	1274.1	1325.7	1376.3	1426.9	1477.8	1529.4	1581.7	1634.7		
	s		1.5706	1.5995	1.6372	1.6599	1.7109	1.7566	1.7984	1.8374	1.8740	1.9066	1.9416		
200	v		2.361	2.585	2.726	3.060	3.380	3.693	4.002	4.309	4.613	4.917			
	h		1210.3	1246.5	1268.9	1322.1	1373.6	1424.8	1476.2	1528.0	1580.5	1633.7			
	s		1.5594	1.6001	1.6240	1.6767	1.7232	1.7655	1.8048	1.8415	1.8763	1.9094			
300	v		1.6638	1.7675	2.005	2.227	2.442	2.652	2.859	3.065	3.269				
	h		1232.5	1257.6	1314.7	1368.3	1420.6	1472.8	1525.2	1578.1	1631.7				
	s		1.5434	1.5701	1.6268	1.6751	1.7184	1.7582	1.7954	1.8305	1.8638				
500	v		0.9927	1.1591	1.3044	1.4405	1.5715	1.6996	1.8256	1.9504					
	h		1231.3	1298.6	1357.0	1412.1	1466.0	1519.6	1573.4	1627.6					
	s		1.4919	1.5588	1.6115	1.6571	1.6982	1.7363	1.7719	1.8056					
700	v		0.7934	0.9077	1.0108	1.1082	1.2024								
	h		1280.6	1345.0	1403.2	1459.0	1513.9								
	s		1.5084	1.5665	1.6147	1.6573	1.6963								
1000	v		0.5140	0.6084	0.6878	0.7604	0.8294	0.8962	0.9615						
	h		1248.8	1325.3	1389.2	1448.2	1505.1	1561.3	1617.3						
	s		1.4450	1.5141	1.5670	1.6121	1.6525	1.6897	1.7245						
2000	v		0.2489	0.3074	0.3532	0.3935	0.4311	0.4668							
	h		1240.0	1335.5	1409.2	1474.5	1536.2	1595.1							
	s		1.3783	1.4576	1.5139	1.5603	1.6012	1.6384							
3000	v		0.0984	0.1760	0.2159	0.2476	0.2757	0.3018							
	h		1060.7	1267.2	1365.0	1441.3	1510.0	1574.3							
	s		1.1966	1.3690	1.4439	1.4984	1.5437	1.5837							



TABLE 9

VALVE FLOW COEFFICIENTS  $C_v$   
CLASS 300 STD. RATING

Valve Size	DEGREES OF DISC OPENING								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
1 1/2"	1	3	6	10	15	22	29	34	38
2"	2	4	9	15	23	34	43	51	57
3"	6	14	29	50	77	111	143	167	188
4"	12	30	63	107	165	238	307	359	404
6"	32	81	167	285	441	635	818	957	1076
8"	40	100	206	352	545	783	1010	1183	1329
10"	71	178	367	628	971	1398	1800	2108	2369
12"	110	276	570	975	1509	2172	2797	3276	3681
14"	136	341	704	1204	1863	2661	3454	4045	4545
16"	169	422	873	1492	2309	3323	4280	5012	5632
18"	247	617	1276	2181	3374	4856	6255	7325	8230
20"	286	714	1476	2524	3906	5620	7240	8478	9526
24"	375	938	1939	3315	5129	7381	9508	11135	12511
30"	715	1788	3696	5319	9776	14068	18121	21221	23644
36"	1104	2760	5704	9752	15087	21711	27967	32751	36799
42"	1711	4279	8843	15118	23390	33659	43358	50774	57050
48"	1867	4667	9645	16490	25513	36713	47292	55381	62226

Table 10  
FLOW COEFFICIENTS  $C_v$   
CLASS 600 STD. RATING

Valve Size	DEGREES OF DISC OPENING								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
3"	5	16	31	51	84	122	151	169	182
4"	8	23	43	70	116	169	209	234	252
6"	26	78	147	242	397	579	717	803	864
8"	35	104	197	324	532	775	960	1076	1157
10"	62	185	350	576	947	1379	1709	1915	2059
12"	85	255	481	793	1302	1897	2350	2633	2831
14"	104	312	589	971	1595	2323	2878	3225	3468
16"	128	383	723	1192	1958	2851	3532	3958	4256
18"	152	456	862	1420	2332	3397	4208	4715	5070
20"	175	524	990	1630	2678	3960	4831	5413	5821
24"	349	1046	1977	3256	5349	7791	9651	10814	11628



HYDRODYNAMIC TORQUE  
OF  
HIGH PERFORMANCE TRUNNION VALVES

The increased use of High Performance Trunnion (Offset Butterfly) Valves used increased use in high flow applications and therefore, a need for accurate prediction of the Hydrodynamic Torque behavior of this type valve. Improper actuator sizing, structural damage and control instability are possible consequences of using inaccurate Hydrodynamic Torque data.

The Trunnion Valve is essentially a modified butterfly valve with the stem offset from the disc sealing surface. See Figure 1. Normally, this type of valve exhibits high opening and closing torques with operating torque appreciating as the valve disc rotates 90° to the fully open position. On occasions where a considerable quantity of fluid is being pumped through the valve, the Hydrodynamic Torque may exceed the opening torque or to such an extent magnitude that the actuator will be unable to further open the valve.

Recognizing the importance of having accurate Hydrodynamic Torque data, Posi-Seal International, Inc. in North Stonington, Conn. launched an extensive program in order to obtain this data. At Posi-Seal's new Hydraulics Laboratory (See Figure 2 for schematic of lab), Hydrodynamic Torque data was taken on valve sizes -1 1/2" through 14" for valve classes 150 through 900. Additional data was taken on a 14" - 900 and a 14" - 1500 lb. valve. Recorded for both preferred and non-preferred fluid flow, measured in 10 degrees of valve rotation. In order to obtain the Hydrodynamic factors, the valve torque was measured while both opening and closing. By averaging the above data, stem packing and bearing friction were negated and pure Hydrodynamic Torque was obtained. The above torque when divided by the differential pressure across the valve gave the Hydrodynamic Torque factor for that particular valve at that location. This data was statistically analyzed on Posi-Seal's

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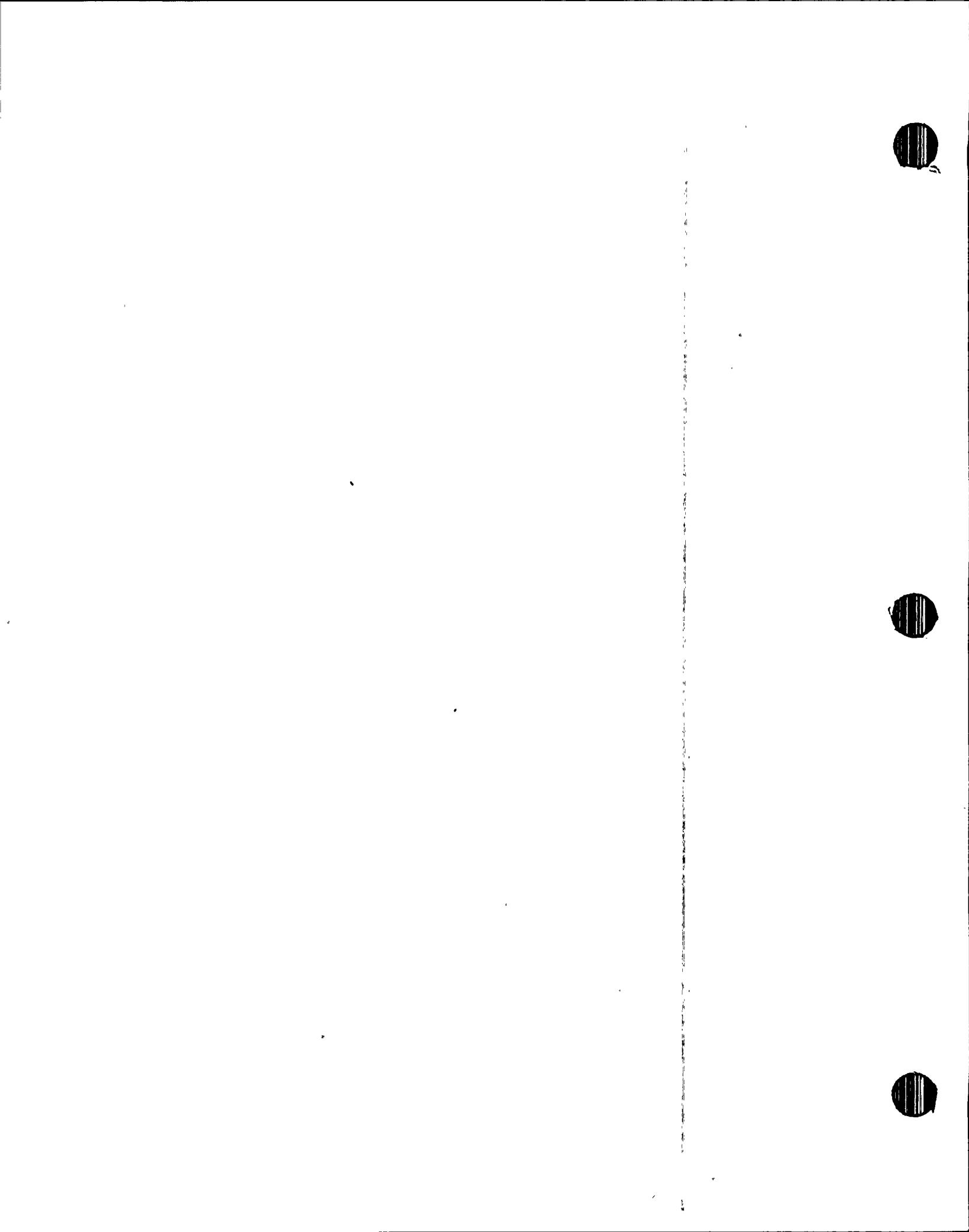
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$$F_D = C_D \rho \frac{AV^2}{2} \quad (\text{Drag})$$

$$\text{and } F_L = C_L \rho \frac{AV^2}{2} \quad (\text{Lift})$$

Where:

$C_D$ ,  $C_L$  - Drag and lift coefficients which are related to the geometry of flow obstruction. (Disc)

$\rho$  - density of the fluid medium

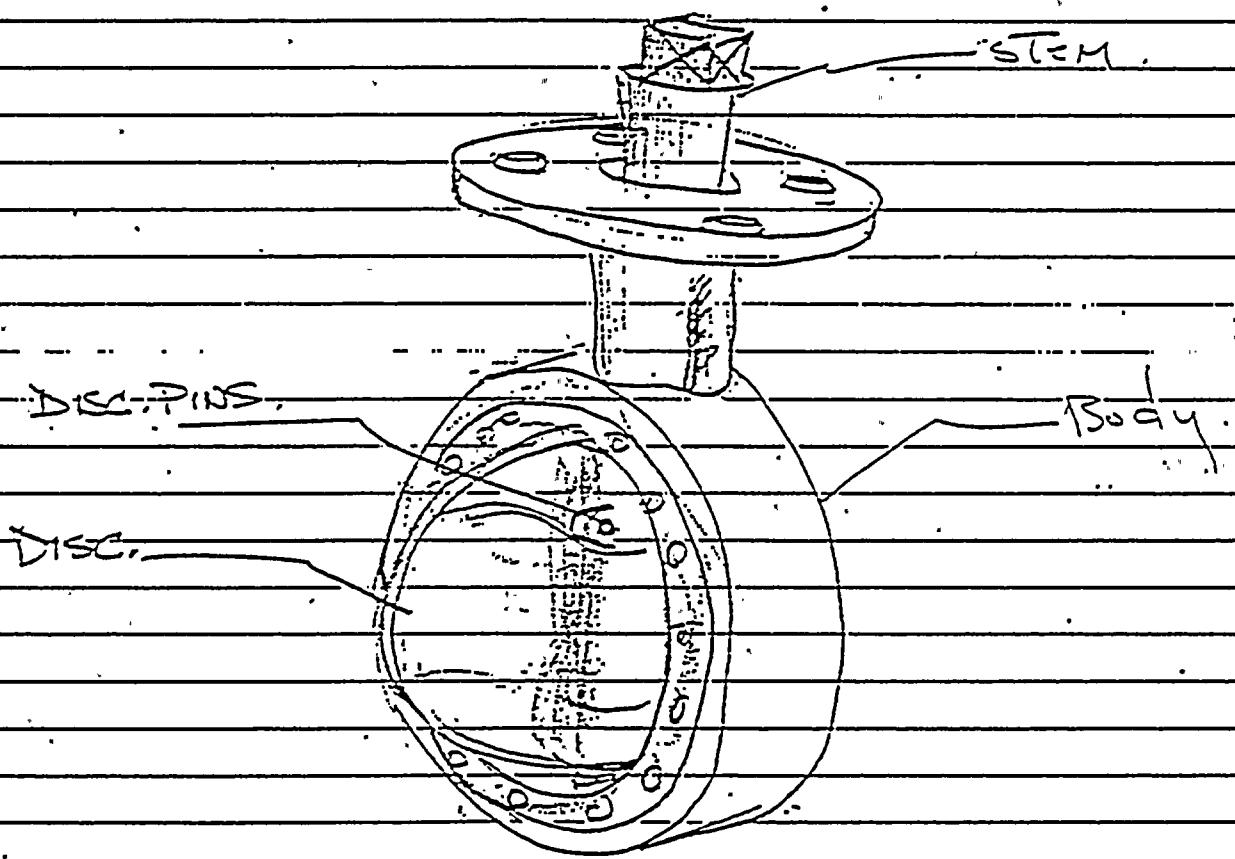
A - projected or surface area of flow obstruction (Disc)

V - velocity of fluid medium

Both the lift and drag forces are dependent upon the shape of the valve disc, its orientation to the flow stream and the direction of fluid flow. As the valve angle is decreased, or flow is reversed, both the magnitude and location of these forces shift causing a change in the resultant Torque. As the valve angle is further decreased the drag forces will increase while the lift forces will deteriorate due to increased turbulence and a breakdown of the flow stream along the downstream side of the valve disc. See Figures 5 and 6.



FIGURE No.: 1  
SCHEMATIC  
OF  
HIGH PERFORMANCE TRIMON VALVE



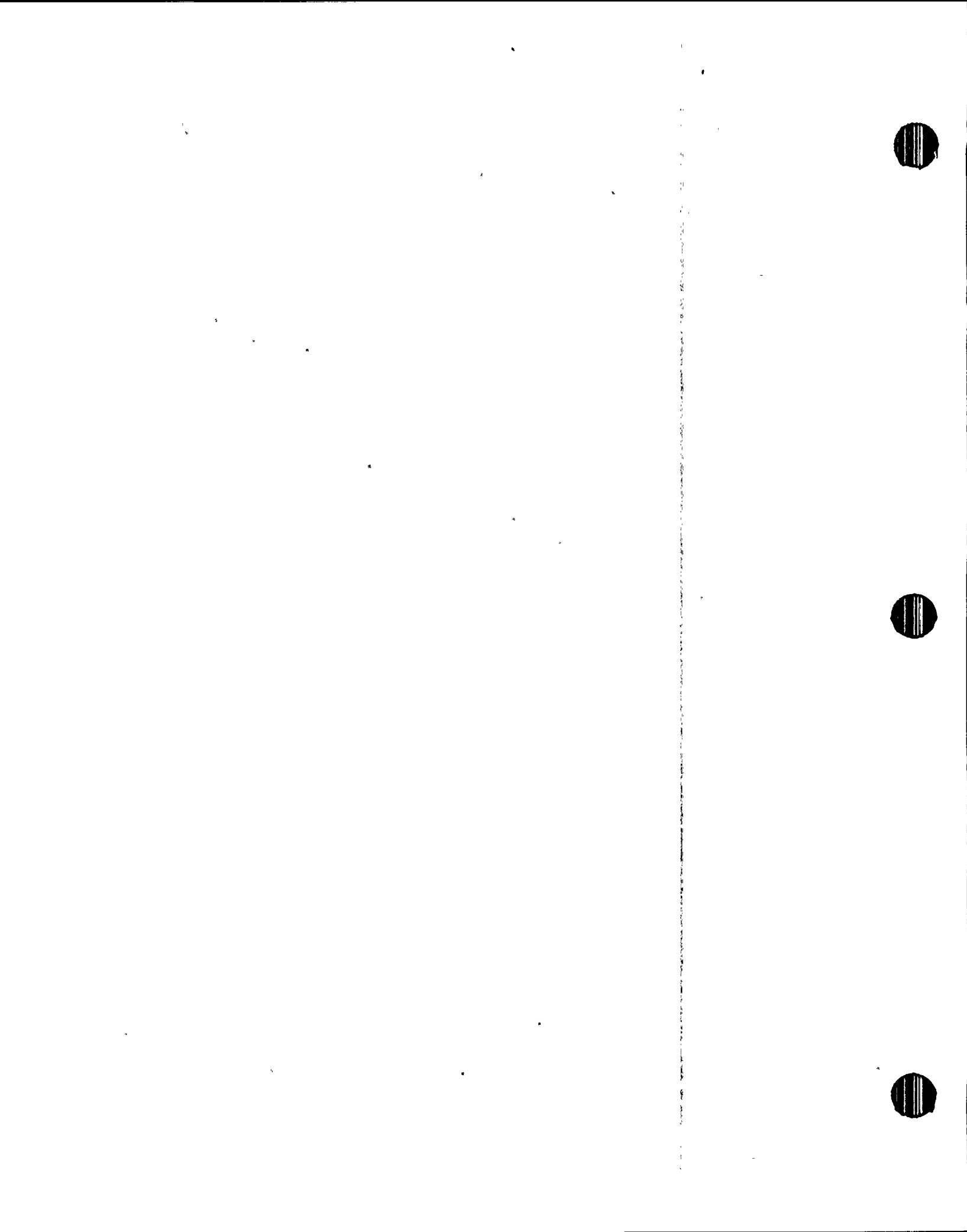
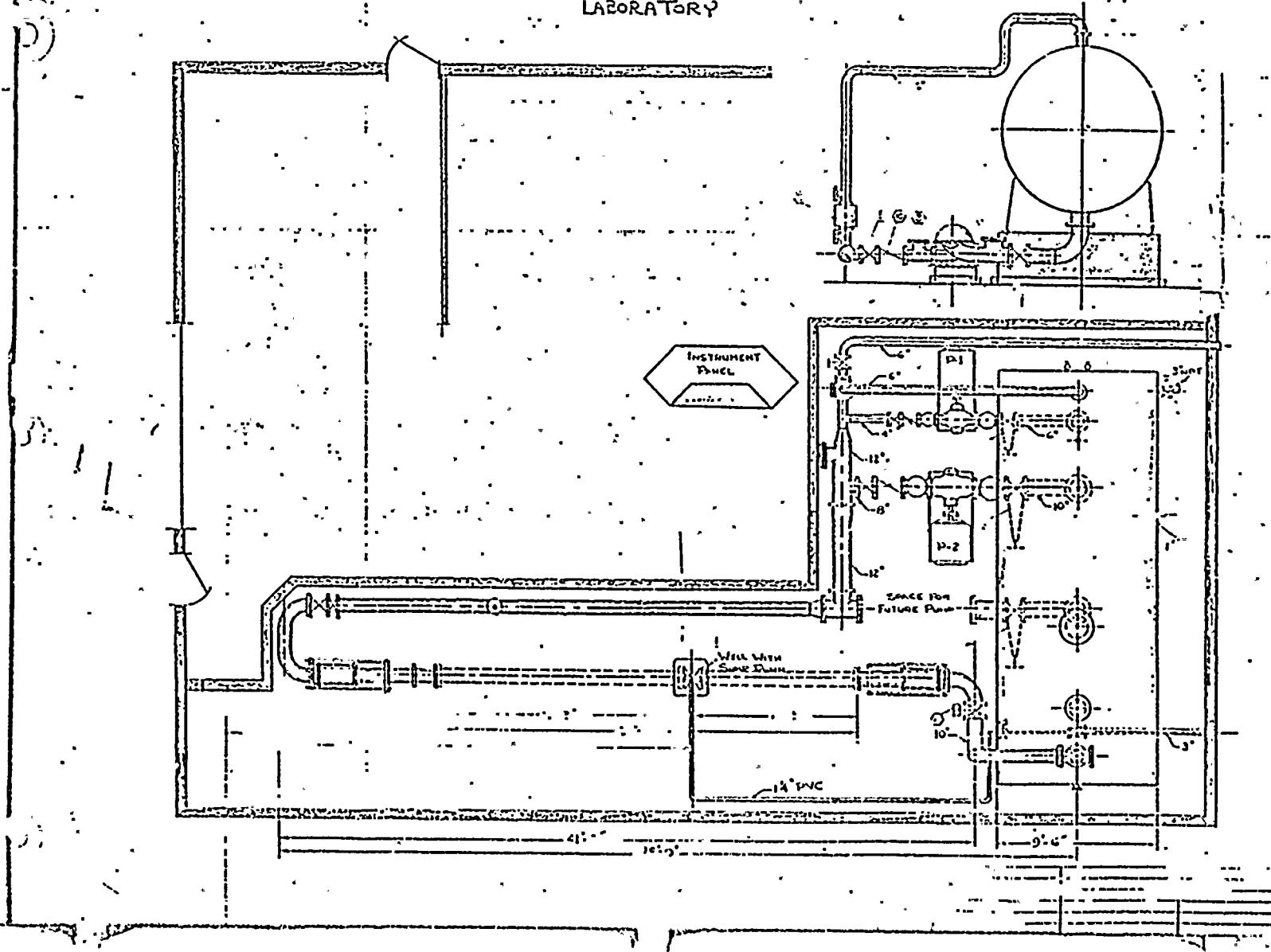
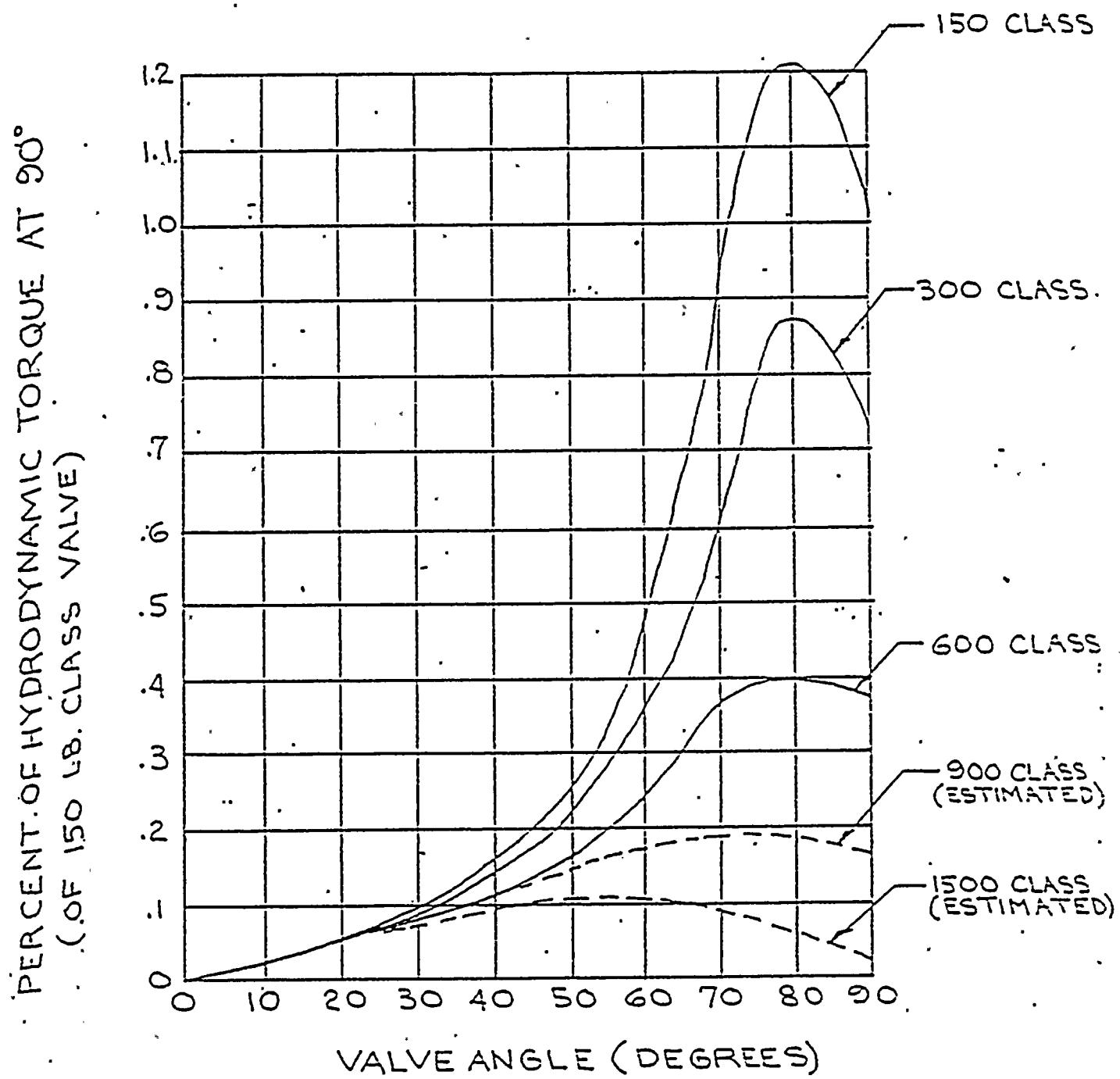


FIGURE NO.: 2  
SCHEMATIC OF POST-SEAL  
RESEARCH & DEVELOPMENT  
LABORATORY





HYDRODYNAMIC TORQUE  
VS  
VALVE ANGLE

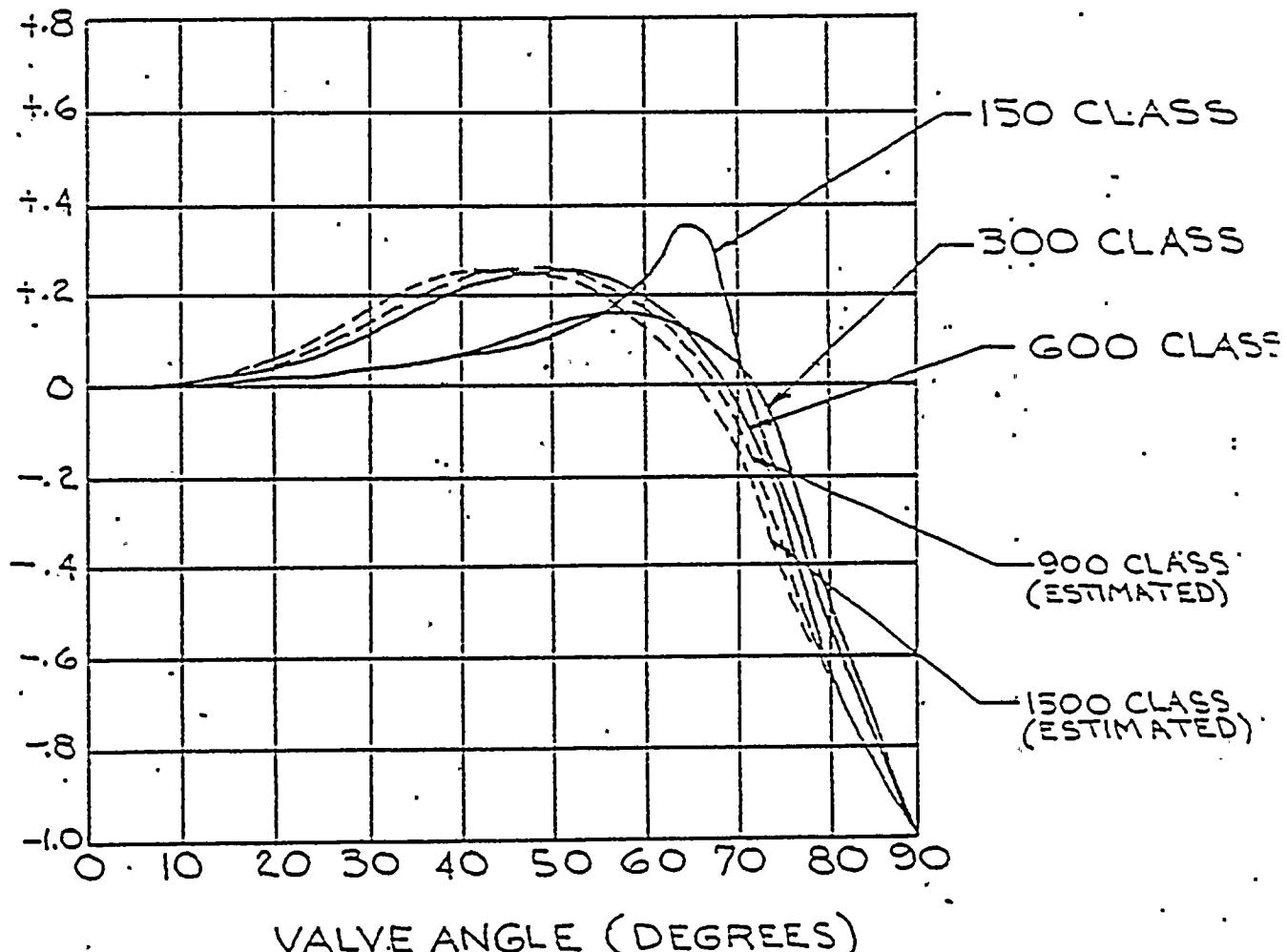


PREFERRED  
DIRECTION



PERCENT OF HYDRODYNAMIC TORQUE AT 90°

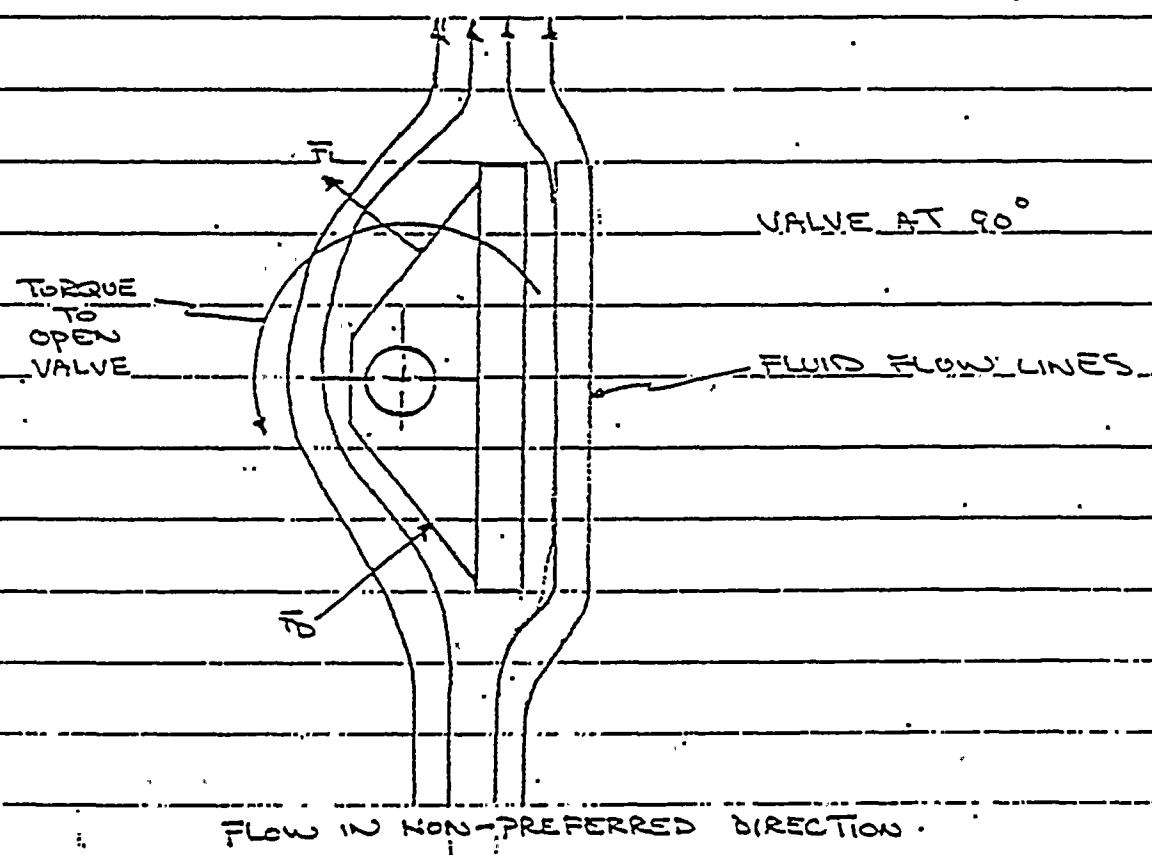
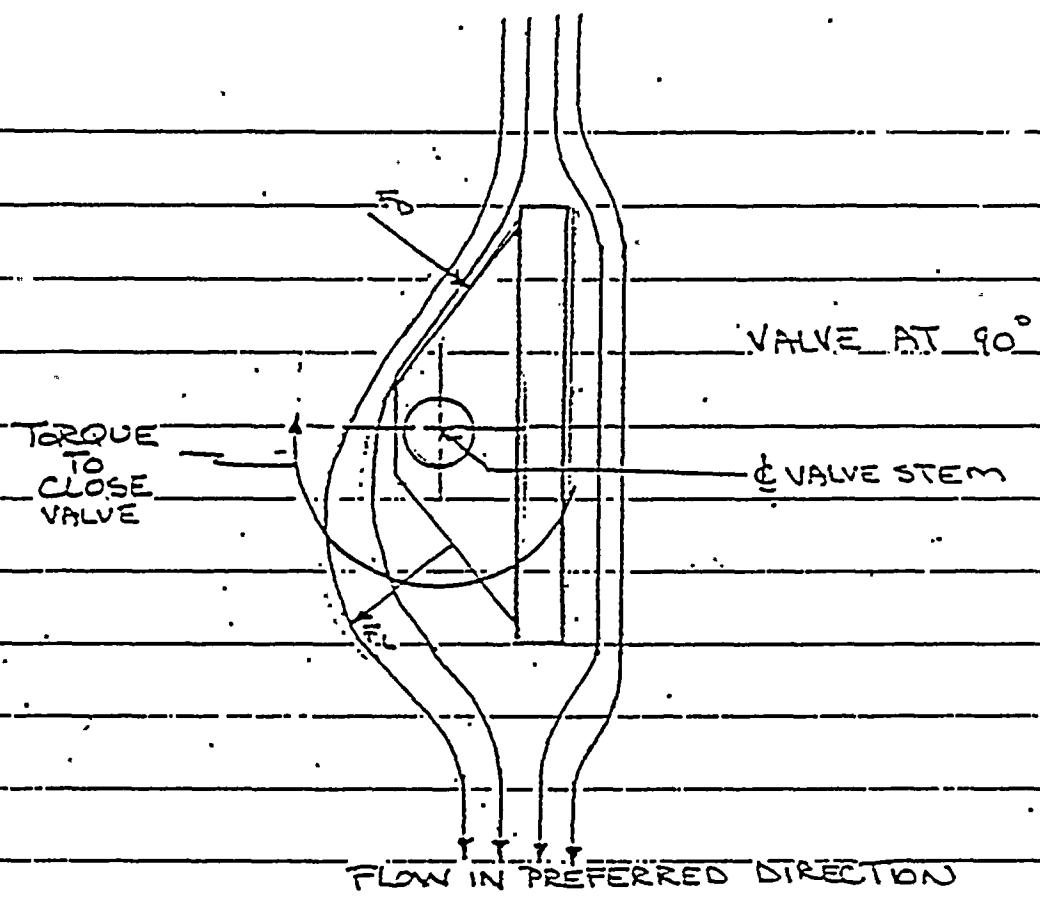
HYDRODYNAMIC TORQUE  
VS  
VALVE ANGLE



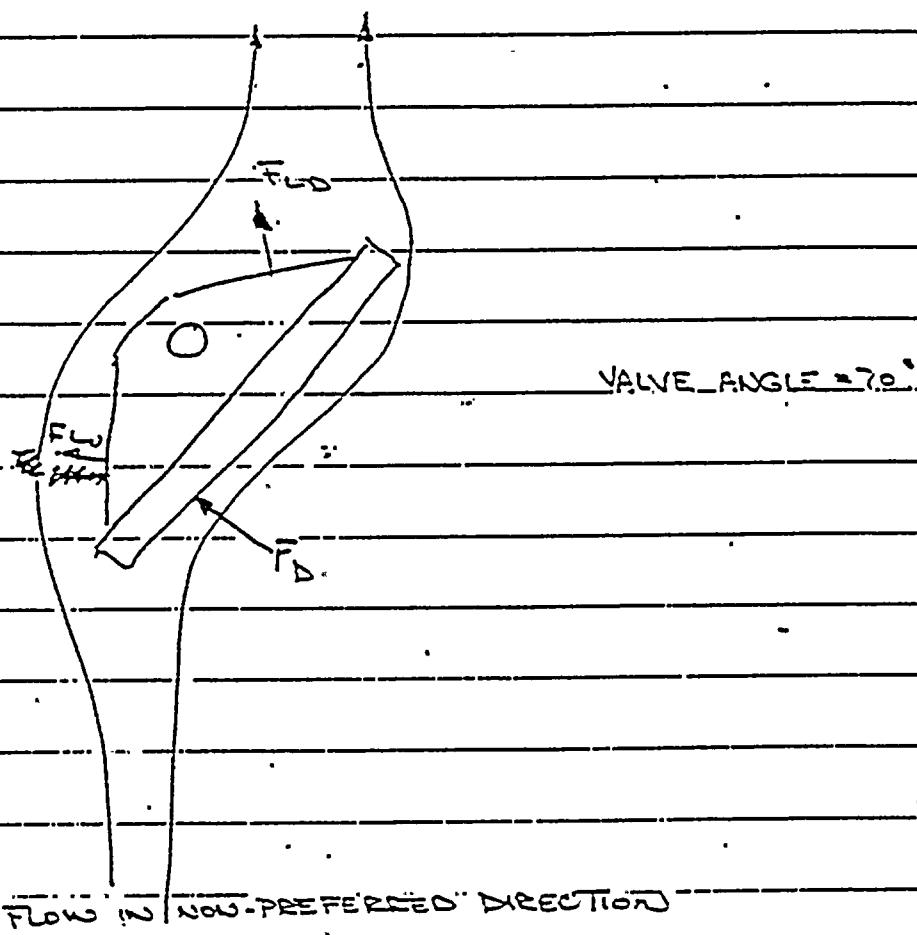
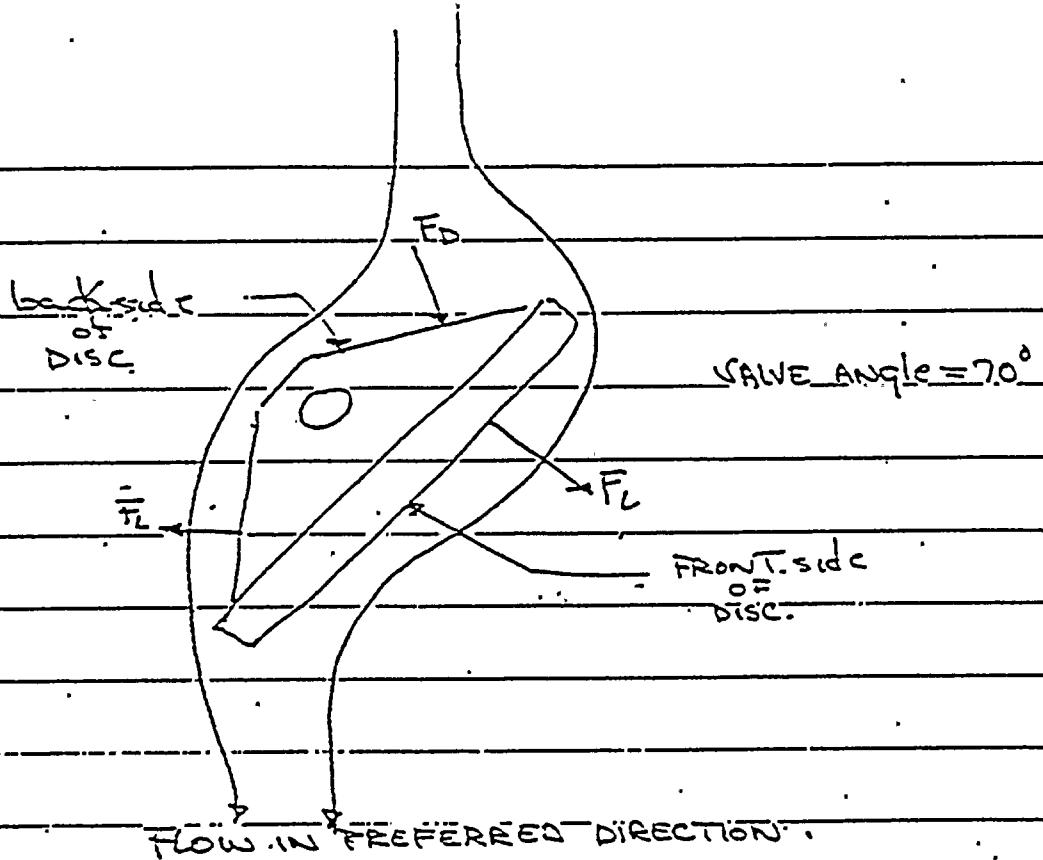
VALVE ANGLE (DEGREES)

NON PREFERRED  
DIRECTION











SHAPE FACTOR VS. POWER FACTOR

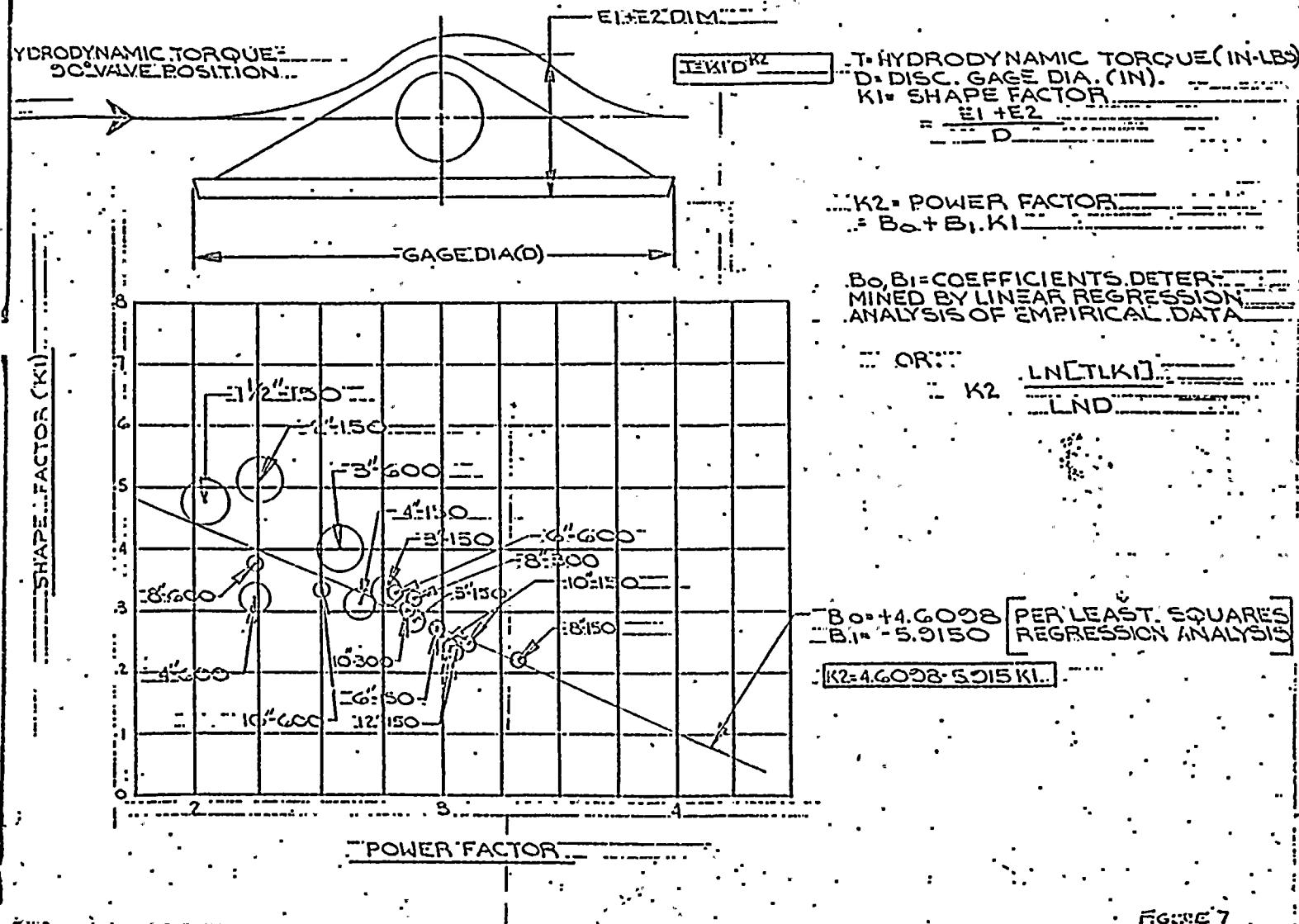


FIGURE 7



HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By John DATE: 12/12/77 Checked By \_\_\_\_\_

VALVE SIZE: 3" ISO

VALVE DIRECTION: STEM UPSTREAM / ~~STEM DOWNSTREAM~~

VALVE SEAL TYPE: TEFLO/N BURST

WATER TEMPERATURE (TANK): 68 °F

DISC TYPE: EDWG

VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE	
				+ TENDING TO CLOSE	- TENDING TO OPEN IN-LB
0				+45	-4.1
10		42		+55	-4.3
20		41		+60	-4.5
30		39		+75	-2.1
40		36		+85	-2.6
50		33		+100	-3.2
60		31.5		+140	-5.2
70		27	27	+140	-125
80		22		+155	-7.0
90		19		+140	-7.4
				+120	-6.7
				+140	-6.4
				645 X	-110
				+100	-2.9
				+80	-1.9
				+60	-1.5
				+30	0.7
				+10	0.2
				0	0
0			21		

PACKING TORQUE: 40 IN-LB OPENING

75 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

NON-PREFERRED DIRECTION

Page

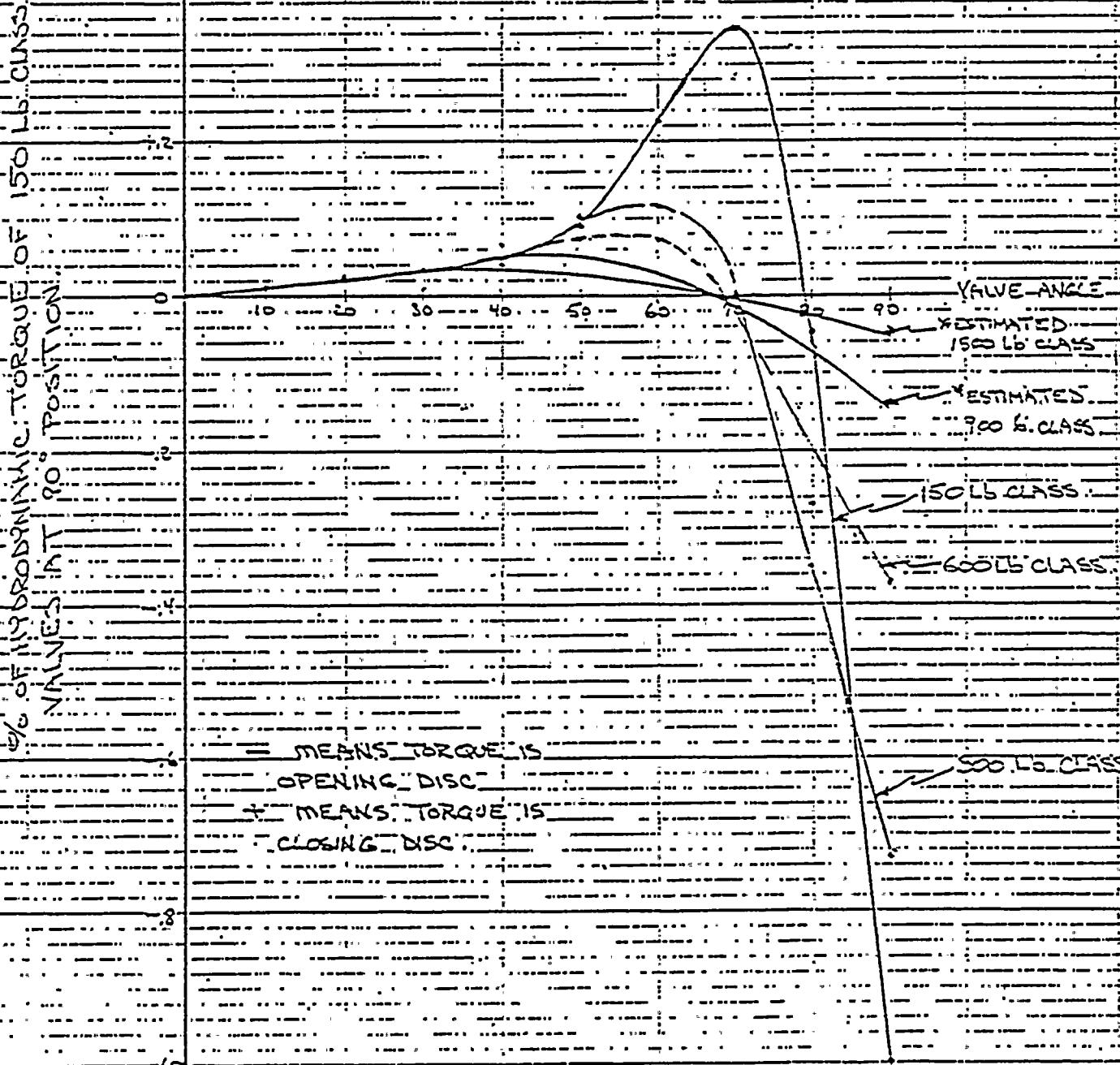
By

Checked By

HYDRODYNAMIC TORQUE

VS.

VALVE ANGLE





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

le : NON PREFERRED DIRECTION

Page

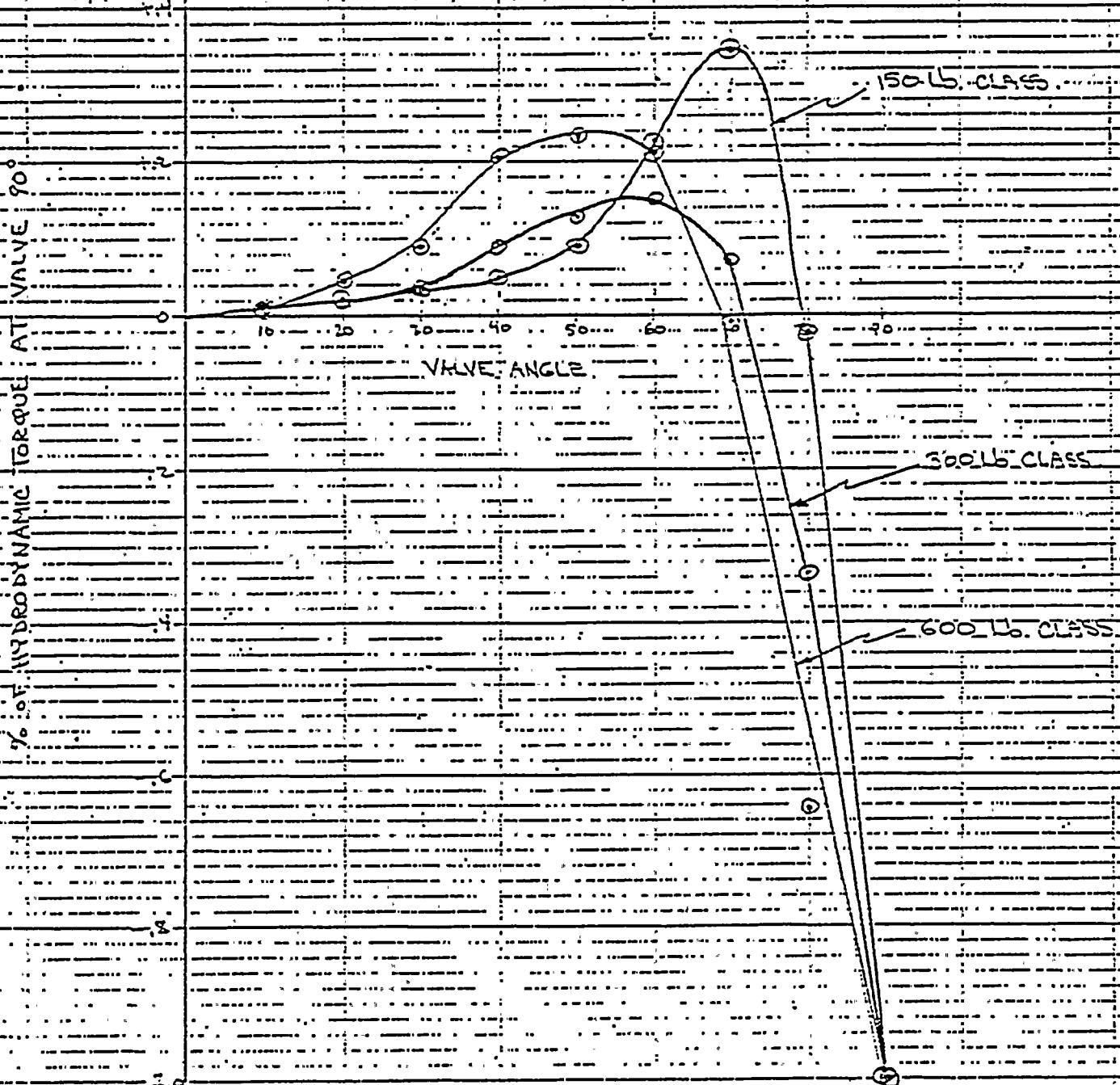
Calc. By

Checked By

HYDRODYNAMIC TORQUE

VS.

VALVE ANGLE





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUES

Calc. By NON-PREFERRED DIRECTION

Checked By DANSEN

Page

8/15/78

ANGLE

VALVE SIZE % TORQUE @ 90°

	10 = 150	8 = 150	12 = 150	Avg.
90	(-378.5)	(-117.8)	(-448.5)	-250
	-1.0	-1.0	-1.0	
80	(-17.2)	(-38.7)	(+20.5)	-1.016
	.309	.217	.054	
70	(-112)	(+63.35)	(+18.05)	+3.345
	+2.96	+3.56	+1.315	
60	(+94)	(-32.55)	(+118.5)	+1.228
	+2.48	+1.83	+1.293	
50	(-47.5)	(+15.05)	(+30)	+1.083
	+1.15	+0.85	+0.79	
40	(+15.5)	(-8.35)	(+25)	+1.05
	+0.41	+0.47	+0.62	
30	(-14)	(-4.775)	(+21.5)	+1.037
	+1.037	+0.27	+1.056	
20	(+2)	(+3.125)	(+24)	+1.025
	+0.005	+0.018	+0.051	
10	(0)	(+2.165)	(+2)	+0.005
	+0	+0.012	+0.004	

11

11

11

POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUES

Page

Calc. By NON-PREFERRED DIRECTION Checked By DANSEN 8/2/78

ANGLE	VALVE SET	% OF TORQUE C-50°			
	5°/150	6°/150	8°/300	10°/300	Avg.
90	-40.95 (-1.0)	-65.1 (-1.0)	-107.3 (-1.0)	-217 (-1.0)	-2.0
80	0 (0)	-28.9 (-.444)	-34.25 (-.291)	-133 (-.613)	-3.37
70	+4.335 (+.106)	+1.3 (+.021)	+420.85 (+.194)	-55 (-.025)	-0.74
60	+3.91 (+.055)	+6.55 (+.101)	+21.4 (+.199)	+44.5 (+.255)	+1.15
50	+13.75 (+.034)	+4.7 (+.063)	+23.8 (+.221)	+40.5 (+.187)	+1.27
40	-27 (-.007)	-43.7 (-.057)	-118.5 (-.110)	-15.5 (+.071)	-0.83
30	-585 (-.014)	-73.25 (-.055)	-76.25 (-.052)	-11.1 (+.065)	-0.25
20	-45 (-.011)	-5 (-.008)	-45.35 (-.050)	-1 (-.005)	-0.09
10	-645 (-.016)	+4.6 (+.011)	+1.65 (-.015)	-2 (+.009)	-0.020



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title : HYDRODYNAMIC TORQUES

Page

Calc. By NON-PREFERRED DIRECTION Checked By DANSEN E/16/78

ANGLE	VALVE SIZE = % OF TORQUE AT 90°			
	6"	8"	10"	Avg.
90	-46.775	-75	-129.45	
	(-1.0)	(-1.0)	(-1.0)	(-1.0)
80	26.57	-52.5	-101.2	
	(-0.5)	(-1.7)	(-1.81)	6.41
70	-2.93	-82.5	-18.5	
	(-0.63)	(-1.1)	(-1.08)	-.007
60	-11.93	-13.1	-28.75	
	(-0.255)	(-1.15)	(-1.22)	-.217
50	-72.435	-17.1	-28.855	
	(-1.26)	(-1.228)	(-1.223)	-.239
40	8	+18.05	-25.9	
	(+.151)	(+.24)	(+.2)	-.204
30	-.191	.14.65	-49.1	
	(-.004)	(+.195)	(-.015)	-.09
20	-3.1095	-13.9	-276	
	(-.066)	(-.185)	(-.021)	-.046
10	-2.212	-7.2	-4.15	
	(-.047)	(+.095)	(-.009)	-.021

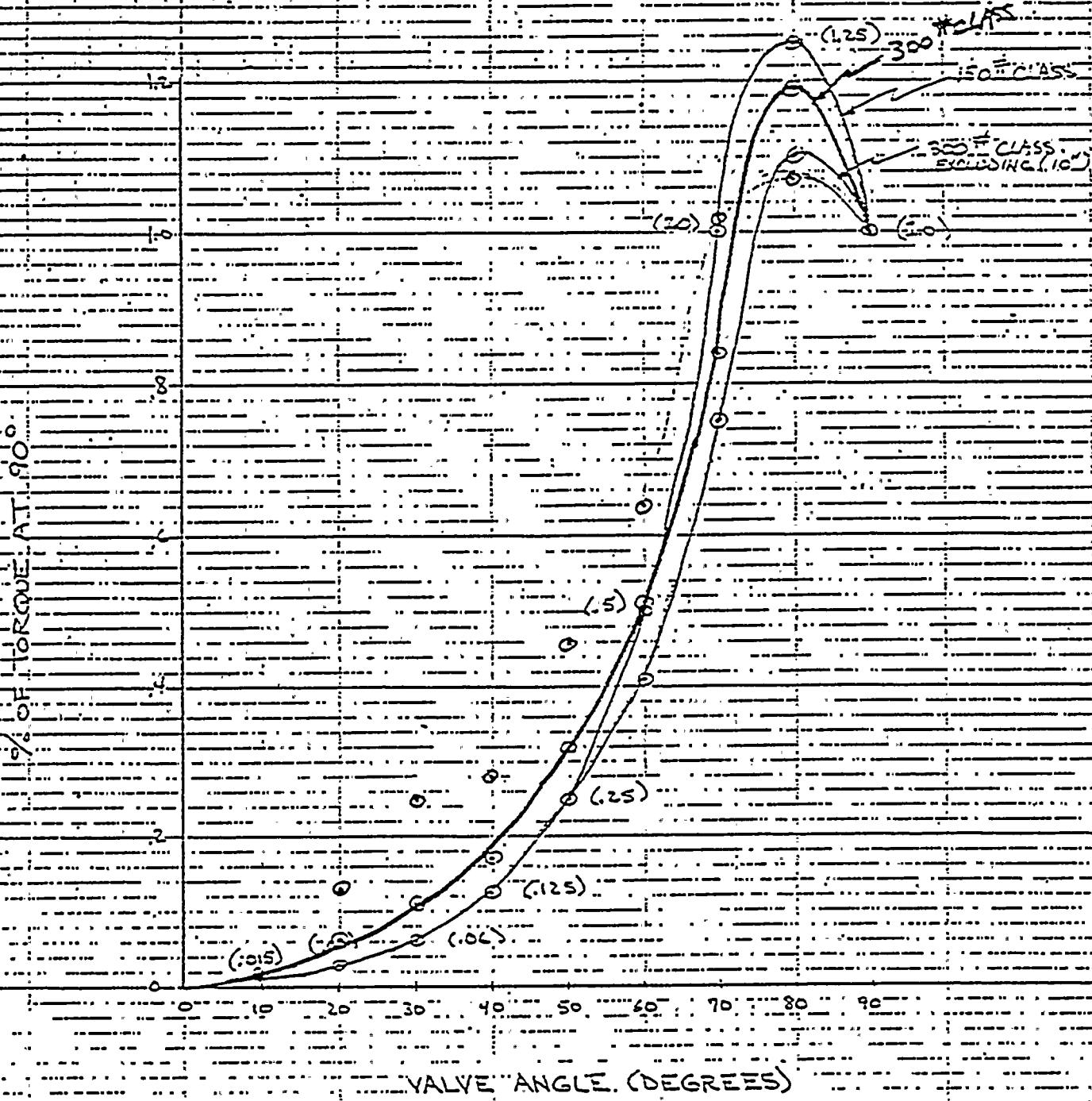


POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Calc. By PREFERRED DIRECTION. Checked By DANSEN 8/8/78

Page

HYDRODYNAMIC TORQUE  
VS.  
VALVE ANGLE





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUES

Page

Calc. By PREFERRED DIRECTION Checked By ØANSEN 8/8/78

ANGLE	VALVE SIZE	% TORQUE @ 90°	Avg.
60°	600	800	105000
45°	(.75) *	(.75) *	
90°	1.0	1.0	1.0
80°	(.62)	(.91)	(138.5)
70°	.98	1.22	1.02
60°	(.37)	(.101)	(134.55)
50°	.71	1.35	1.02
40°	(.168)	(.615)	(100.2)
30°	.35	.53	.74
20°	(.96)	(.464)	(76.8)
10°	.20	.62	.57
40°	(.64)	(.256)	(52.1)
30°	.13	.34	.38
20°	(.56)	(.28)	(36.8)
10°	.12	.37	.27
20°	(.36)	(.94)	(24.2)
10°	.08	.13	.18
20°	(.75)	(.4)	(4.65)
10°	.02	.01	.03
		?	

\*BASED ON NON PREFERRED DIRECTION.



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUES

Calc. By PREFERRED DIRECTION Checked By CANSEN 8/2/78 Page 1

ANGLE	VALVE SIZE = % TORQUE @ 90°				
	5" / 150	6" / 150	8" - 300	10" - 300	Avg (60) Avg (Ex 1050)
(28)	(54.62)	(9545)	(480)	317	
90	1.0	1.0	1.0	1.0	1.0
30	(30 → )	(44.4)	(103.6 → )	(271.5 → )	
	1.07	1.14	1.08	1.5	1.09
70	(1.8 → )	(41.15)	(77 → )	(205.5)	
	.64	.75	.81	1.14	.84
60	(1.9 → )	(2764)	(39.2)	(141)	
	.32	.51	.41	.78	.505
50	(1.52)	(1.9)	(30.3)	(.79)	
		<del>45</del>	.32	.44	.32
40	(3.35)	(8.54 → )	(18.1 → )	(6.39 → )	
	.12	.16	.19	.22	.17
30	(2.05)	(6.32)	(9.6 → )	(22.5)	
	.07	.12	.10	.13	.10
20	(1.15)	(4.35)	(4.35)	(13.5 → )	
	.04	.08	.05	.08	.06
10	(-.465)	(-.88)	(3.5 → )	(4.5 → )	
	.02	.02	.04	.03	.02
					.01

\* 5" & 6" = 150# ARE EQUIVALENT TO 300# CLASS VALVES



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

## Hydrodynamic Torques

Page

Calc. By PREFERRED DIRECTION Checked By OANSEN 8/7/78

ANGLE

VALVE STATE = % TORQUE @ 90°

ANGLE	10° = 150 <sup>(1)</sup>	12° = 150 <sup>(2)</sup>	8° = 150 <sup>(3)</sup>	10° = 150 <sup>(4)</sup>	12° = 150 <sup>(5)</sup>	Avg.
90	(245)	667.1(333)	(24)	(37)	(55)	
90	1.0	1.0	1.0	1.0	1.0	1.0
80	(32)	(425)	(15)	(34)	(424)	
80	1.27	1.25	1.25	1.03	1.25	1.22
70	(227)	(345)	(83)	(234)	(322)	
70	.93	1.04	.57	.74	.92	.91
60	(122)	(186)	(--)	(115)	(163)	
60	.50	.56		.37	.52	.49
50	(59)	(104)	(--)	(59)	(77)	
50	.24	.31		.16	.22	.24
40	(30)	(87)	(--)	(32)	(34)	
40	.32	.26		.10	.10	.15
30	(-16)	(33)	(--)	(25)	(24)	
30	.07	.10		.08	.07	.08
20	(-9)	(-26)	(--)	(14)	(18)	
20	.03	.08		.04	.05	.05
10	(-3)	(-11)	(--)	(8)	(--)	
10	.05	.03		.02	.03	.02

(?)  
DELETE  
NOT GOOD  
DATA



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By Dawn Date: 12/16/77 Checked By: \_\_\_\_\_

VALVE SIZE: 150

VALVE DIRECTION: STEAM TO STEAM SYSTEM DOWNSTREAM

VALVE SEAL TYPE: TEFLO/N/BUNA

WATER TEMPERATURE (TANK): 68° OF

DISC TYPE &amp; Dwg:

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB	(14) / 145 145
0					
10		43		+45	1.0
20		41		+45	1.1
30		38.5		+40	1.6
40		36		+45	1.3
50		32		+55	1.7
60		35		+60	1.7
70		25		0	0
80		19		-75	3.9
90		23		90	3.9
		23		90	3.9
		18.5		-75	4.5
		21		-40	1.9
		27.5		-10	0.4
CLOSING		36		+10	0.3
		28.5		0	0.0
		30.5		-15	0.5
		32		-15	0.5
		32		-15	0.5
0					

PACKING TORQUE: 20 IN-LB OPENING

10 IN-LB CLOSING



Title S-1500 HYDRODYNAMIC TORQUE CURVE

Page \_\_\_\_\_

Calc. By C. Green (STEM UP STREAM) Checked By \_\_\_\_\_

8

7

6

5

TORQUE

PSI

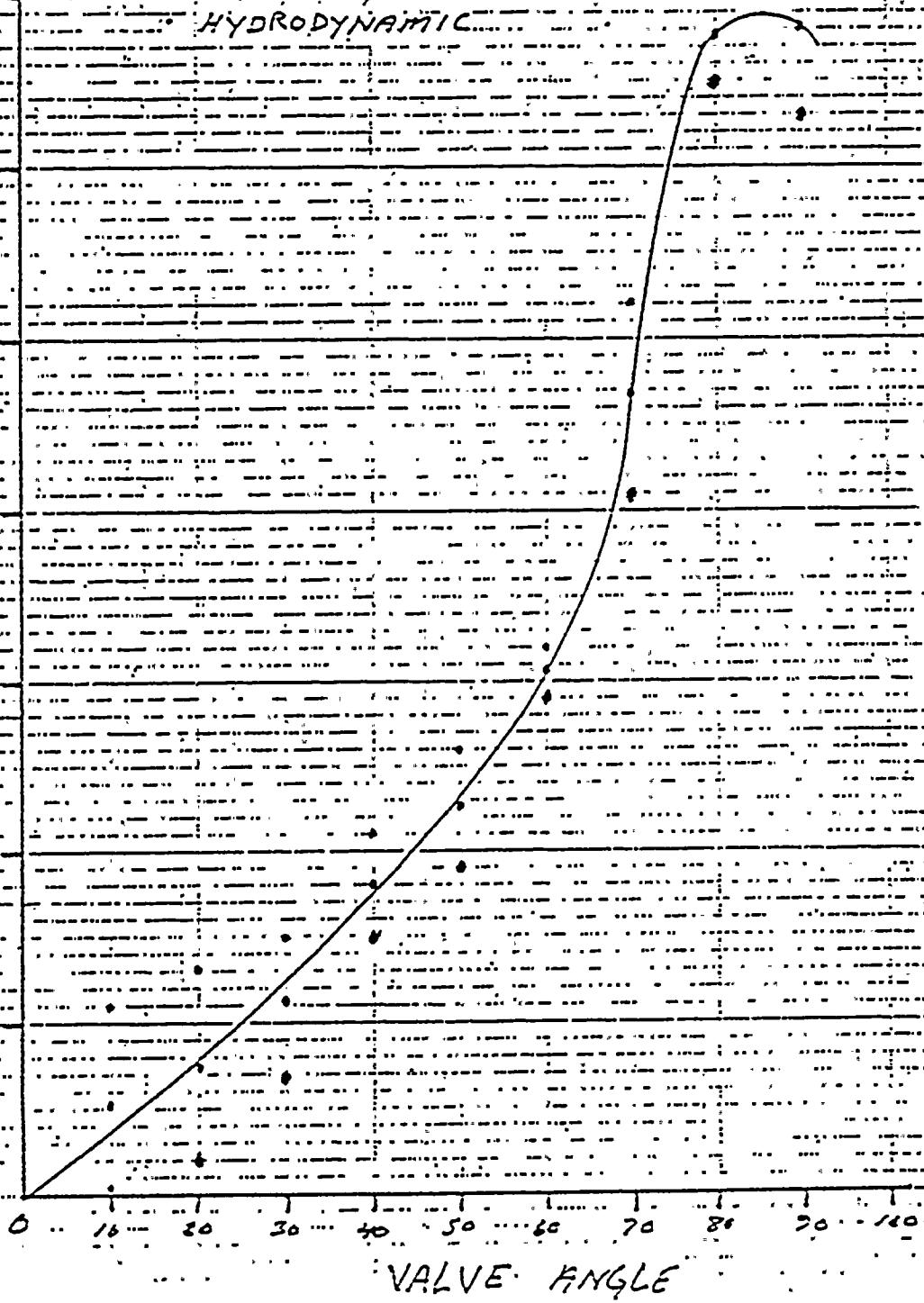
4

3

2

1

- CLOSING
- OPENING
- HYDRODYNAMIC





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title 3"-150LB - HYDRODYNAMIC TORQUE CURVE Page \_\_\_\_\_  
Calc. By C. Livors, (stem downstream) Checked By \_\_\_\_\_

2



0

1

2

3

4

5

6

• HYDRODYNAMIC  
• CLOSING  
• OPENING

0 10 20 30 40 50 60 70 80 90 100



HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Scl. By Dave DATE: 2/5/77 Checked By \_\_\_\_\_VALVE SIZE: 4-150VALVE DIRECTION: STEM UPSTREAM *(open backflow)*VALVE SEAL TYPE: TEFLON/BONWATER TEMPERATURE (TANK): 65 °F

DISC TYPE &amp; DWG.

OPENING	VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB	1.07 1.76 2.03 2.42 3.12 4.90 8.00 13.04 14.37 8.82 11.36 7.57 4.63 2.70 1.43 1.10 0 -1.55
	0	46.5	42.5	37	31	
10					+75	
20					+75	
30					+75	
40					+75	
50					+100	
60					+125	
70					+140	
80					+150	
90					+125	
90					+75	
80					+125	
70					+125	
60					+125	
50					+85	
40					+50	
30					+40	
20					0	
10					-60	
0						
CLOSING						

PACKING TORQUE: 5 IN-LB OPENING5 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page 3

Ac. By Ray Marshall DATE: 11-17-77 Checked By \_\_\_\_\_

VALVE SIZE: 4"-150

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TETRON/RING

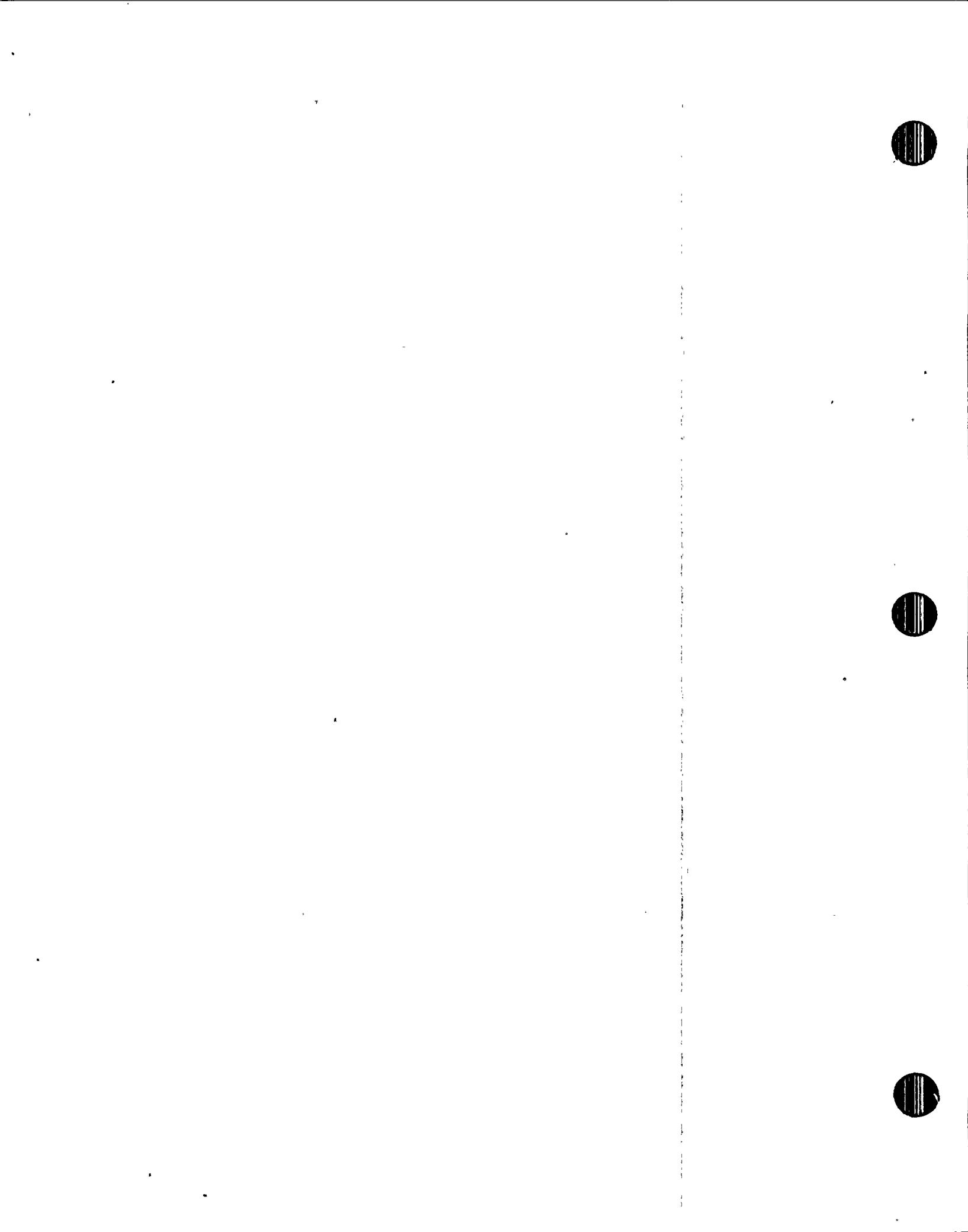
WATER TEMPERATURE (TANK): 60° F

DISC TYPE & Dwg:

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP, PSI	Q, GPM	TORQUE + TENDING TO CLOSE IN-LB	TORQUE - TENDING TO OPEN IN-LB
0		X		X	
10		30.5		+75+40	1.31
20		32		+40	1.25
30		30.5		+45	1.47
40		30.5		+60	1.97
50		35		+80	2.23
60		27		+50	1.85
70		18		+49	2.72
80		11		-10	-0.91
90		8.5		-55	-6.47
		X		X	
90		8.7		-80	-9.2
80		11		-30	-2.73
70		17.5		0	0
60		27		+15	.56
50		35		+45	1.29
40		43.5		+25	.57
30		29.5		+10	.34
20		29		-5	.17
10		28		0	0
0		X		X	

PACKING TORQUE: 10 IN-LB OPENING

5 IN-LB CLOSING

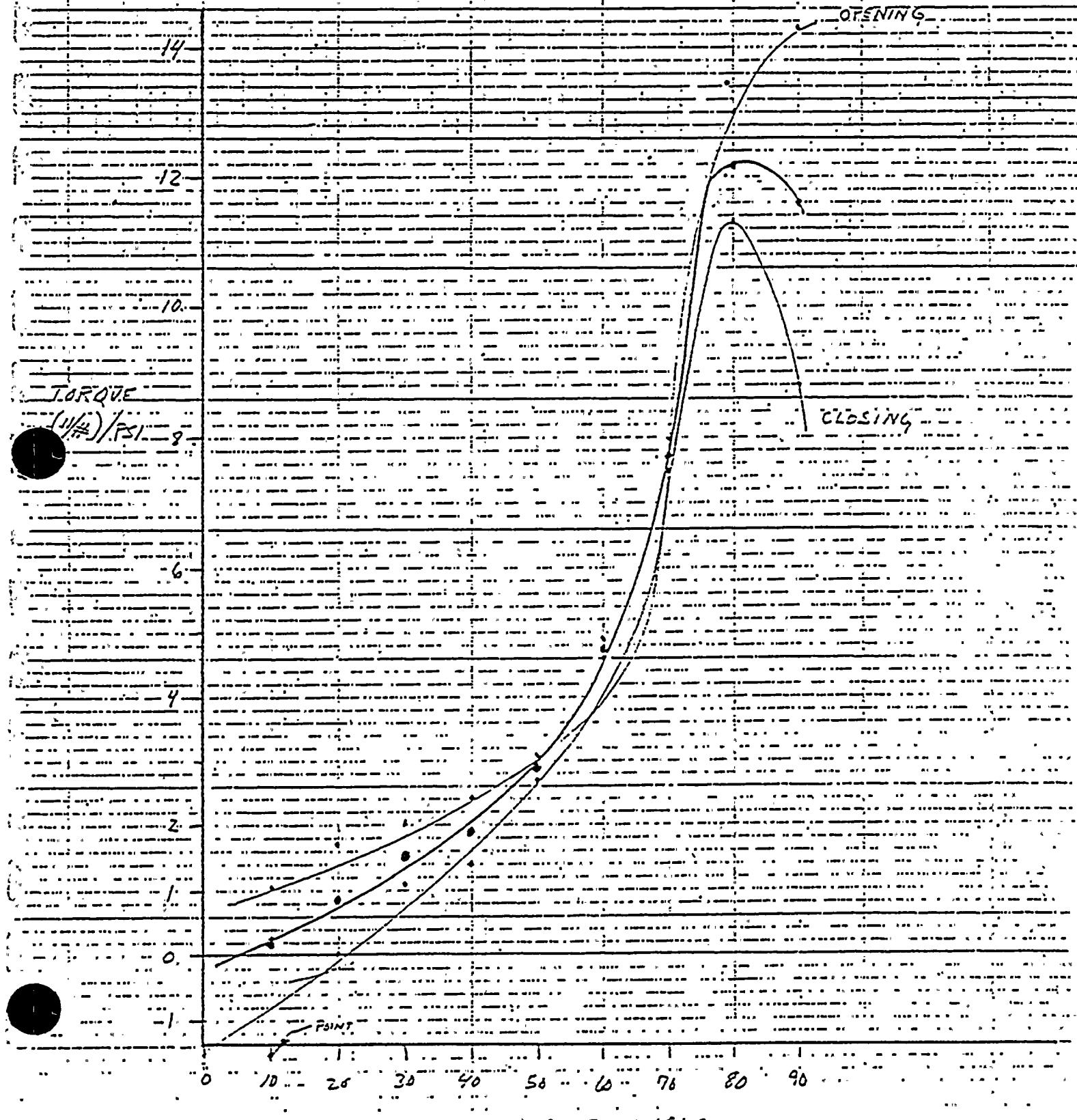


## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

Title 4" 150# HYDRODYNAMIC TORQUE CURVE

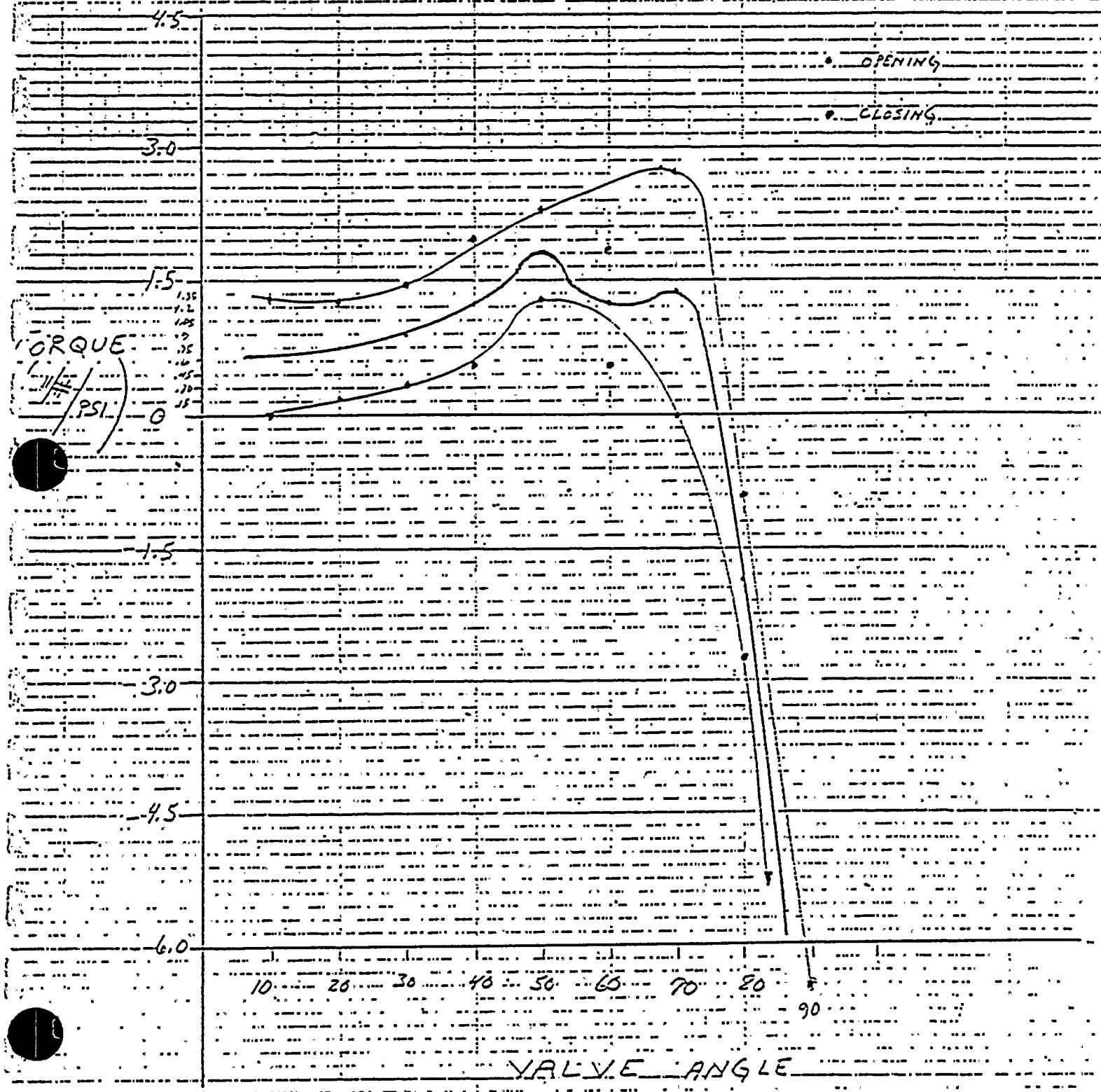
Page \_\_\_\_\_

Calc. By C. LIVORSI (STEM UPSTREAM) Checked By \_\_\_\_\_



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title 4"-150LB-HYDRODYNAMIC TORQUE CURVE Page 2 of  
Calc. By C. Liverst. (STEM DOWN STREAM) Checked By





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Ac. By T.C.R.Y. DATE: \_\_\_\_\_ Checked By: \_\_\_\_\_

CONST. UPSTREAM PRESS.

VALVE SIZE: 6" 650 - 300

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TEE / GUNA

WATER TEMPERATURE (TANK): 37° F

DISC TYPE & DWG: 2

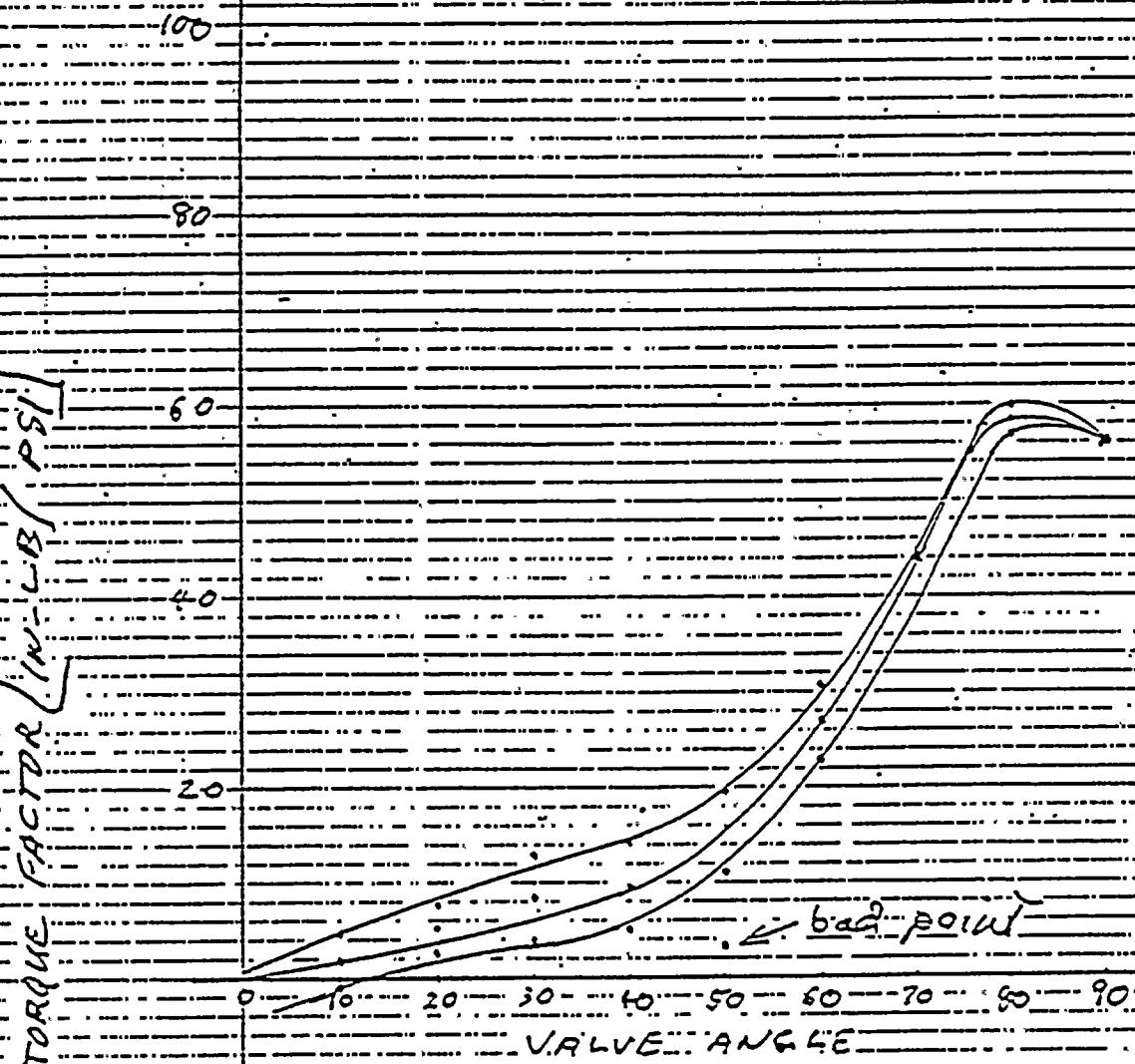
VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB
0				
10	18.1	12		50
20	18.1	14		0
30	18.6	13.5		93.50
40	18.1	13.8		70
45	18.7	15		100
60	18.7	14		300
70	18.8	12.5		500
80	18.3	11.5		700
90	18.1	11		600
90	18.6	12.8		700
80	18.6	12.5		750
70	18.6	12.12		550 700
60	18.6	13		440
45	18.9	15		300
40	18.4	12.5		140
30	18.4	10		125
20	18.3	11.5		100
10	18.1	13.5		80
0				

PACKING TORQUE: IN-LB: OPENING

IN-LB: CLOSING



PERFORMANCE CURVES





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Ac. By \_\_\_\_\_

DATE: \_\_\_\_\_

Checked By \_\_\_\_\_

VALVE SIZE : 6" 150 300

VALVE DIRECTION : STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE : TEFLOK / BURK

WATER TEMPERATURE (TANK) : 66 °F

DISC TYPE & DWG : 2

OPENING	VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB						
		0	10	20	30	40	50	60	70	80	90
	0										
	10		38.5								
	20		4.9								
	30		6.2								
	40		7.8								
	50		8.2								
	60		6.5								
	70		8.75	15							
	80		8.5	11							
	90		4.5	8.3							
	100										
	90		2.1	5.5							
	80		11.5	11							
	70		16.7	16.2							
	60		14.5	12.5							
CLOSING	50		14.5								
	40		12.5								
	30		1.5								
	20		3.6								
	10		50.5								
	0										

PACKING TORQUE : IN-LB OPENING  
IN-LB CLOSING



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

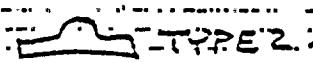
Title HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Ic. By R. OANSEN DATE: 9/20/77 Checked By \_\_\_\_\_

VALVE SIZE: 6" - 150/300

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TEF/BUNA  TYPE 2

WATER TEMPERATURE (TANK): 63° OF

DISC TYPE &amp; DWG:

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP, PSI	Q, GPM	TORQUE TENDING TO CLOSE IN-LB	(IN-LB)/PSI
0		X		X	
10	44.5			+175	3.9
20	30.0			+75	2.5
30	11			+75	6.8
40	11			+90	9.2
50	10.2			+45	4.4
60	9.7			+45	4.6
70	5.7			+15	2.6
80	9.2			-275	-28.0
90	8.4			-550	-62.5
		X		X	
90	8.5			-550	-64.7
80	9.0			-260	-28.9
70	27.5			+240	0.7
60	23.5			+200	8.3
50	22.5			+85	3.8
40	18.5			-15	-0.8
30	19.0			-5	-0.3
20	31.5			-110	-3.5
10	28.5			-150	-5.3
0		X		X	

PACKING TORQUE: 10 IN-LB OPENING

10 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE CURVE Page \_\_\_\_\_  
Calc. By C. LIVORSI (stem down) Checked By \_\_\_\_\_

6" 150 LB

10

10

20

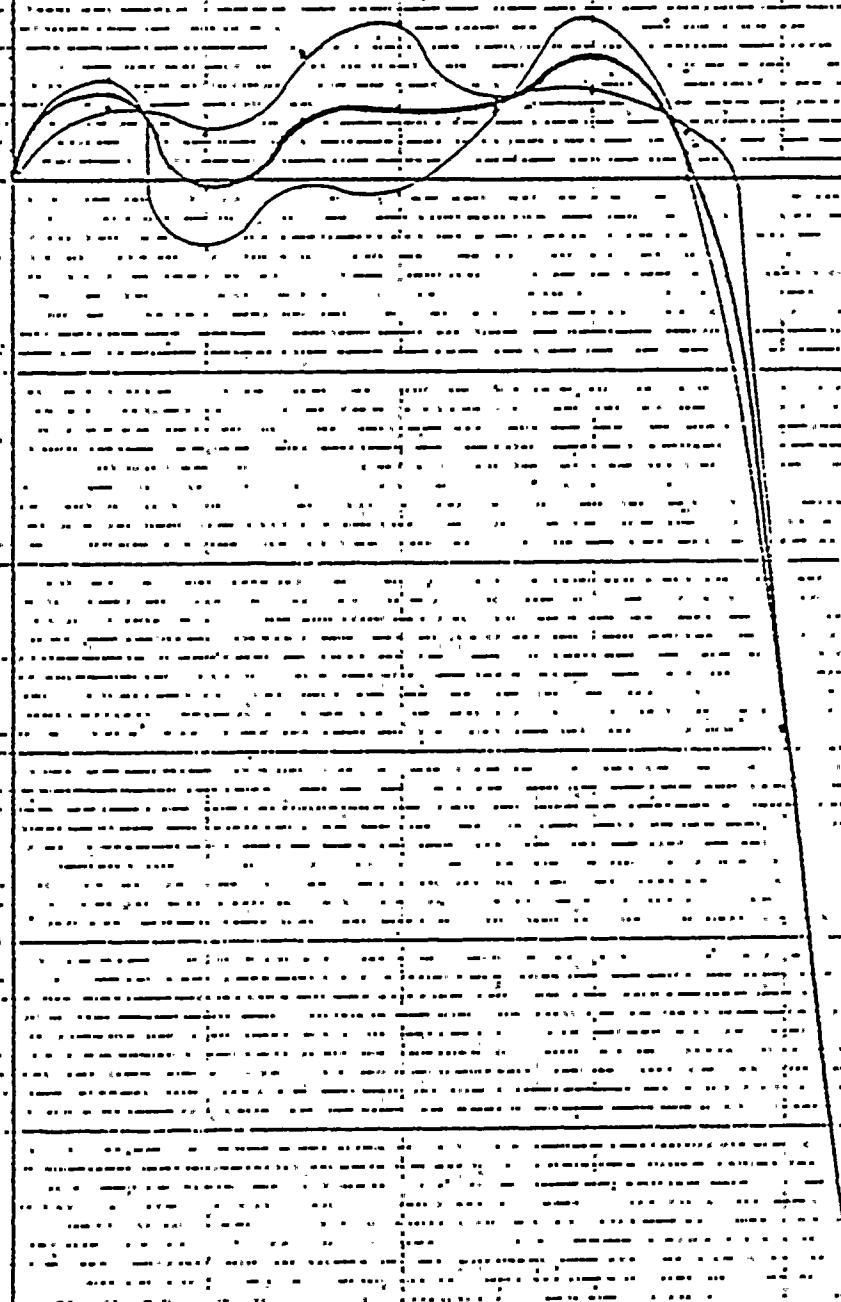
30

40

50

60

0 10 20 30 40 50 60 70 80 90 100





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION

Page 5

Calc. By C. LIVORSII DATE Checked By

VALVE SIZE: 8" ISOLB

VALVE DIRECTION: STEM UPSTREAM

VALVE SEAL TYPE:

WATER TEMPERATURE (TANK): 71 °F

DISC TYPE & DWG:

	VALVE ANGLE DEGREES	P <sub>1</sub> PSIG	ΔP PSI	Q GPM	TORQUE + TENDENCY TO CLOSE - TENDENCY TO OPEN IN-LB	(Y) / (X) OPENING
	0	69.5	65.		400	
	10	59.5	59.		100	1.68
	20	56	56		4.25	7.6
	30	51.5	51.5		5.50	10.7
	40	43	43		725	16.8
	50	31	31		775	25
	60	18	18		740	41.1
	70	8.5	8.5		700	92.3
	80	4.5	4.5		650	144.2
	90	2.5	2.5		600	240
	90	2.0	2.0		375	187.5
	80	3.0	3.0		400	133
	70	6.0	6.0		500	83.3
	60	12.5	12.5		550	44
	50	26.5	26.5		525	21.7
	40	38.5	38.5	37	400	10.6
	30	37.5	37.5	47	350	7.7
	20	41.5	41.5	54	400	7.3
	10	54.5	54.5	54	100	4.8
	0				375	

PACKING TORQUE: 160 IN-LB OPENING

80 IN-LB CLOSING



HYDRODYNAMIC TORQUE DETERMINATION

Page 6

Calc. By C. Lirestine Date Checked By

J. H. Young

VALVE SIZE: 8" 150

VALVE DIRECTION: ~~UPSTREAM~~ / STEM DOWNSTREAM

VALVE SEAL TYPE:

WATER TEMPERATURE (TANK): 70 °F

DISC TYPE EDWA

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB	
	OPENING	CLOSING			
0				900 $\frac{1}{2}$	
10	58			350	6.03
20	56			350	6.12
30	54			375	7.35
40	48			445	10.4
50	28.5			450	15.8
60	15			460	30.7
70	7.5	AP @ 75° = 8.5	42.5 ± 8.5	450	60
80	5.3	AP @ 75° = 6.0	47.5 ± 6.0	410	72.4
90	2.6	AP @ 75° = 4.5	52.5 ± 4.5	450	17.5
			7.0 @ 25° = .01		
90	3.0			550	48.5
80	3.0	AP @ 25° = 2.5	52.5 ± 2.5	0	0
70	7.5	AP @ 25° = 3.6	50.0 ± 3.6	500	66.7
60	10	AP @ 25° = 5.5	52.5 ± 5.5	550	54.4
50	28	AP @ 25° = 3.75	52.5 ± 3.75	400	44.4
40	39.5			250	6.12
30	46			100	2.2
20	54.5			0	0
10	58			100	1.7
0				900 $\frac{1}{2}$	

PACKING TORQUE: 150 IN-LB OPENING

100 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.

ENGINEERING CALCULATIONS

8"-150LB

HYDRODYNAMIC TORQUE (PREFERRED)

Page

Calc. By

C. LIVORSI

Checked By

200

200

100

0 20 40 60 80 100

PSI

0 20 40 60 80 100



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

8=150Title HYDRODYNAMIC TORQUE CURVE (UNPREFERRED) Page \_\_\_\_\_  
Calc. By C. Liverst Checked By \_\_\_\_\_

150

100

50

0

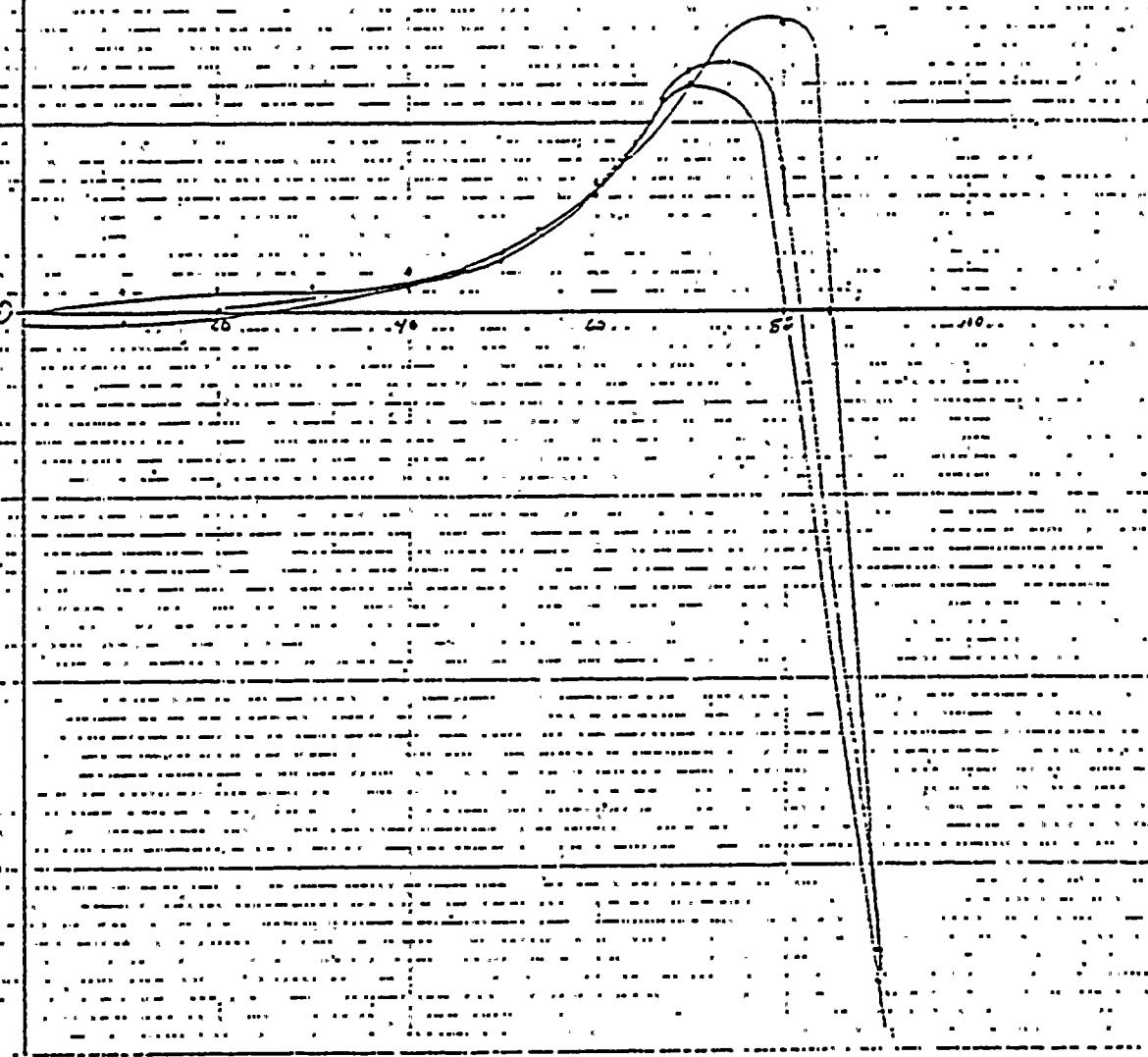
50

100

150

200

60 70 80 90 100





## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION (F1) Page \_\_\_\_\_

Calc. By RO DATE: 6/17/97 Checked By \_\_\_\_\_

VALVE SIZE: 10" &amp; 15"

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TEFILON ISUNA / DISC TYPE: 2

WATER TEMPERATURE (TANK): 58° F

DISC TYPE &amp; DWG

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE		115° FPS
				TENDING TO CLOSE	TENDING TO OPEN	
OPENING	0	54.9	226.51	0	41250 / 1150 / 120	16.5
	10	54.9	50.5	395	850	21.6
	20	30	25.5	895	550	30.4
	30	16	11.5	1030	350	41.7
	40	8.5	3.6	1400	150	60
	50	2.5	1.5	3560	250 - 900	134.9
	60	18.5	6.3	3590	850	250
	70	16.0	3.2	3590	800	363.67
	80	15.0	2.2	3580	800	667
	90	4	0.75	2685	600	1167
	100	4	0.5	2127	390	175
	110	40	1.5	2623	150	125
	120	40	2.0	2863	250	94.7
	130	41	3.0	2820	275	65
	140	41	4.0	2620	300	57.2
	150	42	7.0	2538	350 - 500	22
CLOSING	160	45	17.0	2260	375	10
	170	51	32.0	1800	225	
	180	54	51	1195	0	
	190	61	56	360	0	
	200	61	56	0	0	

PACKING TORQUE: 50 IN-LB OPENING

50 IN-LB CLOSING

111

111

111

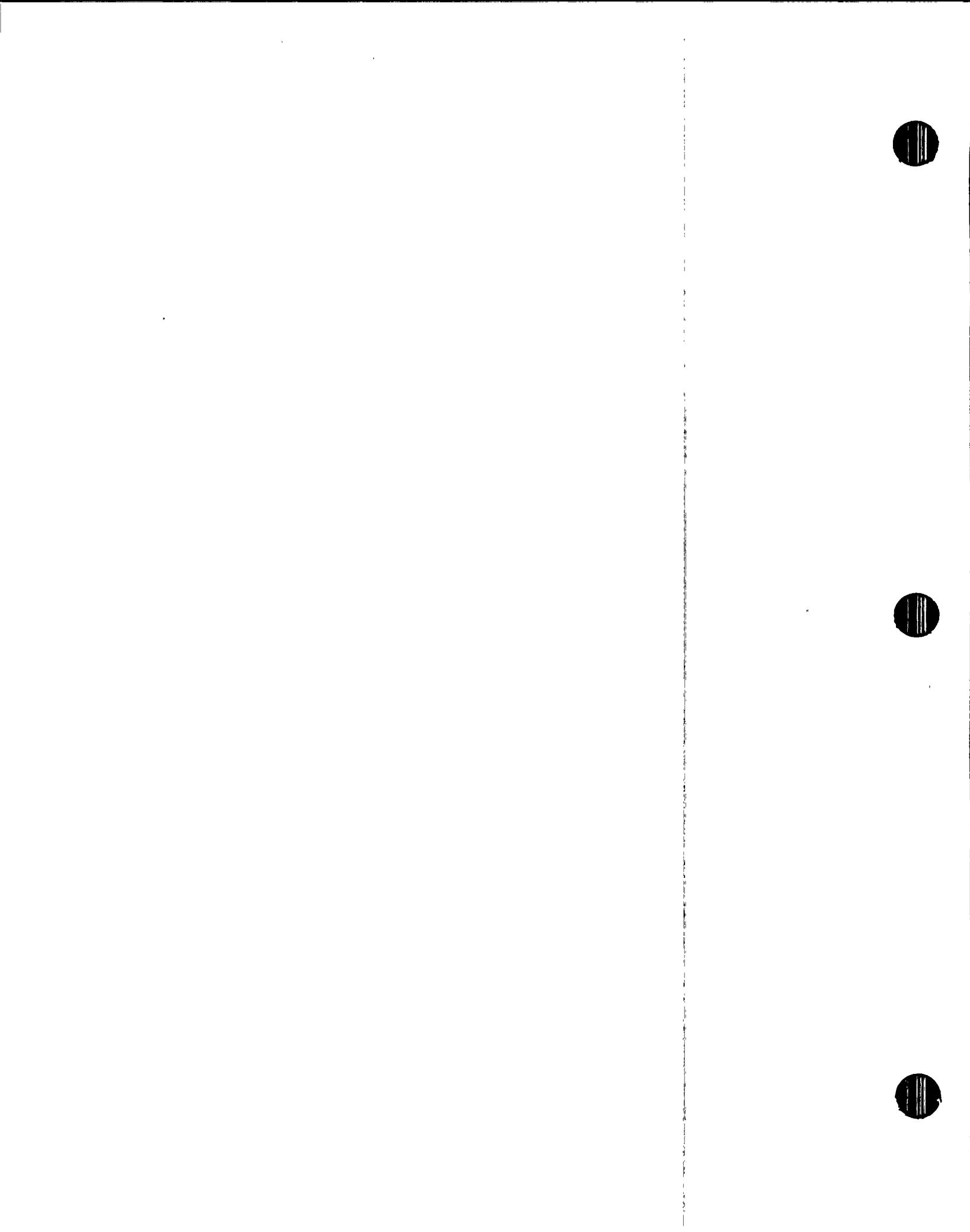
POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION (2)Calc. By J.C. Date 6/17/77 Checked By VALVE SIZE: 10"-150VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAMVALVE SEAL TYPE: TEFLON / BUNA DISC TYPE: 2WATER TEMPERATURE (TANK): 80 °FDISC TYPE: C-DWG

VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB
0	36.9	16.5	218	320
10	44.5	12.43	229	225
20	52.1	10.5	160.518	600 400
30	62.8	9.32	1740	750 225
40	72.2	7.5	2217	400
50	81.6	7.5	2727	450
60	90.2	6.0	3587	750
70	97.6	3.5	3594	700
80	106.6	2.5	3596	700
90	116.0	1.75	3595	450
90	15	0	0	300
80	16.3	2.0	3583	650
70	17.3	3.0	3597	700
60	19.8	6.0	3579	725
50	26.5	7.5	3572	800
40	49.5	14.0	2140	450
30	57.2	11.0	1170	300
20	62.1	14.0	732	300
10	65.9	15.0	311	200
0				

PACKING TORQUE: 50 IN-LB OPENING50 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

#3

Page

Title HYDRODYNAMIC TORQUE DETERMINATION

Calc. By \_\_\_\_\_ Date 6/27/77 Checked By \_\_\_\_\_

VALVE SIZE : 10"-150

VALVE DIRECTION : STEM UPSTREAM / STEM DOWN

VALVE SEAL TYPE : FLON/BONAR

WATER TEMPERATURE (TANK) : 78° F

DISC TYPE & DWG : 2

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB
0	7.5/37.5			
10	45.7/42.3	-33/23.5	300/250	850/-750
20	17.5/45.2	-19.5		700
30	8.5	→		450
40	17.5	→		700
50	7.0	→		575
60	5.0	→		625
70	2.5	→		625
80	2.0	→		725
90	1.5	→		550
90		1.5		400
80		2.0		575
70		3.0		650
60		6.0		600
50		13.0		450
40		26.0/15.5		300/-150
30		23		100
20		23		275
10		33.5		600
0				

PACKING TORQUE : 50 X IN-LB OPENING

50 X IN-LB CLOSING



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATIONPage 4Calc. By W.H.DATE 7/6/77Checked by W.H.

Cavitation measurements - Control valve

Water open

VALVE SIZE: 10" = 150

VALVE DIRECTION: STEM UPSTREAM / STEM downstream

VALVE SEAL TYPE: TEFLO/N / BONFIL

WATER TEMPERATURE (TANK): 77 °F

DISC TYPE &amp; DIA: 2 1/2

OPENING	VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE TENDING TO CLOSE IN-LB	TORQUE TENDING TO OPEN IN-LB
		0	X	6.51	1200	24
	10		4.51		1400	28
	20		5.05		1400	36
	30		4.35		1575	51
	40		2.85		1450	81
	50		1.35		1100	142
	60		0.25		925	275
	70		3.0		825	356
	80		2.25		850	295
	90		2.0		550	214
	90		1.75		375	257
	80		2.25		600	179
	70		3.5		625	96
	60		6.75		650	37
	50		14.25		525	9
	40		29.5		275	4
	30		44.5		200	11
	20		51.5		550	10
	10		58.5		1100	
	0					

PACKING TORQUE: 50 X IN-LB OPENING

50 X IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By Deacon DATE: 6/24/77 Checked By

VALVE SIZE: 10 - 150

VALVE DIRECTION: OPEN UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TEFLO/BSNA

WATER TEMPERATURE (TANK): 76 °F

DISC TYPE & DWG: 2

OPENING	VALVE ANGLE DEGREES	P, UPSTREAM (PSI.G)	ΔP, PSI	Q, GPM	TORQUE
					+ TENDING TO CLOSE
0					-
10		42.5			- 800
20		28			- 650
30		11.5			- 425
40		3.0			- 525
50		10.5			- 700
60		6.5			- 775
70		3.5			- 550
80		1.7			- 175
90		1.7			- 625
					-
					- 700
					- 50
					- 4200
					- 1450
					- 275
CLOSINGS	40	42.885			- 75
	30	16.5/19/30.5			- 50/-50/-27
	20	17.5			- 325
	10	18.5			- 350
	0	0			-

PACKING TORQUE: 50 IN-LB OPENING

50 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By

Date: 6/1/77

Checked By

Full open - Control valve

VALVE SIZE: 10-150

VALVE DIRECTION: DOWNSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TEFILON / Buna

WATER TEMPERATURE (TANK): 80 °F

DISC TYPE & DWG: 2

	VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE TENDING TO CLOSE TENDING TO OPEN IN-LB
OPENING	0				
	10		57.5		+1050
	20		47.7		+850
	30		39.5		+750
	40		26.5		+300
	50		14.5		+725
	60		7.0		+250
	70				
	80				
	90				
CLOSING	90				
	80				
	70				
	60		6.5		+350
	50		13.5		+200
	40		25		0
	30		39.5		-450
	20		51.0		-700
	10		58.5		-800
	0				

PACKING TORQUE: 50 IN-LB OPENING

50 IN-LB CLOSING



## POSI-SEAL INTERNATIONAL, INC.

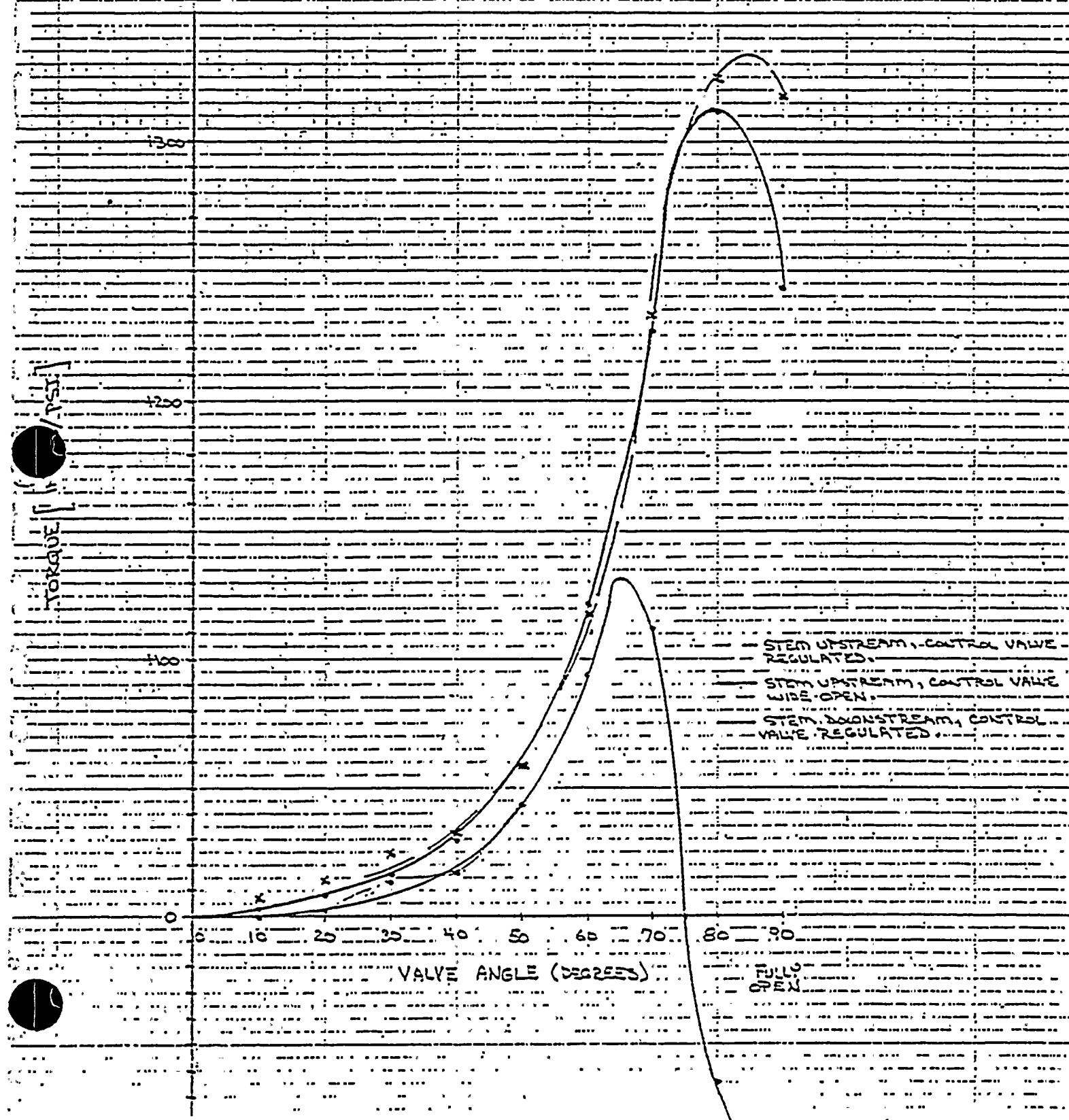
## ENGINEERING CALCULATIONS

Title TORQUE VS. VALVE ANGLE 10'-150

Page

Calc. By R. O'RAISIN

Checked By





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By C. LIVORSKI DATE: Checked By \_\_\_\_\_

VALVE SIZE: TR-150

VALVE DIRECTION:  STEM UPSTREAM /  STEM DOWNSTREAM

VALVE SEAL TYPE: TEFON

WATER TEMPERATURE (TANK): 60° F

DISC TYPE: EDWG

	VALVE ANGLE DEGREES	Δ P (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
OPENING	0				+ TENDING TO CLOSE
	10	50	1400	28	
	20	36.5	1300	36	
	30	20.5	850	41	
	40	13.5	1000	49	
	50	8.5	850	100	
	60	3.5	825	236	
	70	2.3	750	326	
	80	1.5	760	467	
	90	1.0	500	500	- TENDING TO OPEN
CLOSING	90	4.0	200	200	
	80	1.6	460	460	
	70	1.5	475	517	
	60	3.5	750	129	
	50	8.0	475	53	
	40	17.5	325	19	
	30	36.5	225	6	
	20	48.5	0	0	
	10	55	550	10	
	0				

PACKING TORQUE: 150 IN-LB OPENING

200 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION

Page 2

Calc. By C. Liroks DATE 10/10/85 Checked By \_\_\_\_\_

VALVE SIZE: 12" 150

VALVE DIRECTION:  STEM UPSTREAM /  STEM DOWNSTREAM

VALVE SEAL TYPE: TEFILON

WATER TEMPERATURE (TANK): 60° F

DISC TYPE & DWG:

VALVE ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
OPENING	0	55	1000	+ TENDING TO CLOSE
	10	47.5	950	-
	20	25	900	-
	30	17	550	-
	40	12.5	350	-
	50	8	400	-
	60	5.5	650	-
	70	3.8	600	-
	80	2.2	600	-
	90	1.2	300	-
CLOSING	90	1.2	0	-
	80	1	350	-
	70	1.4	500	-
	60	2.2	500	-
	50	3.4	550	-
	40	4.5	550	-
	30	5.5	350	-
	20	6.6	450	-
	10	7.5	50	-
	0	6.2	1200	-

PACKING TORQUE: 150 IN-LB OPENING

: 150 IN-LB CLOSING



HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By : C. Liversi Date : 7-7-78 Checked By \_\_\_\_\_

VALVE SIZE : 12" - 150

VALVE DIRECTION :  STEM UPSTREAM /  STEM DOWNSTREAM

VALVE SEAL TYPE : TEFILON

WATER TEMPERATURE (TANK) : 67 °F

DISC TYPE - EDWG

VALVE ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE (IN-LBS)	IN-LBS	COMENTS
OPENING	0	62	7000	+ TENDING TO CLOSE
	10	27	550	-
	20	5	300	-
	30	10	450	-
	40	7.7	450	-
	50	5.5	350	-
	60	4.0	650	-
	70	1.9	450	-
	80	1.2	200	-
	90	.8	300	-
CLOSING	90	.8	450	-
	80	1.8	100	-
	70	4.6	200	-
	60	4.0	300	-
	50	9.5	100	-
	40	16	0	-
	30	30	50	-
	20	44	550	-
	10	53	1150	-
	0	63	100	-

PACKING TORQUE : 725 IN-LB OPENING

750 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.

ENGINEERING CALCULATIONS

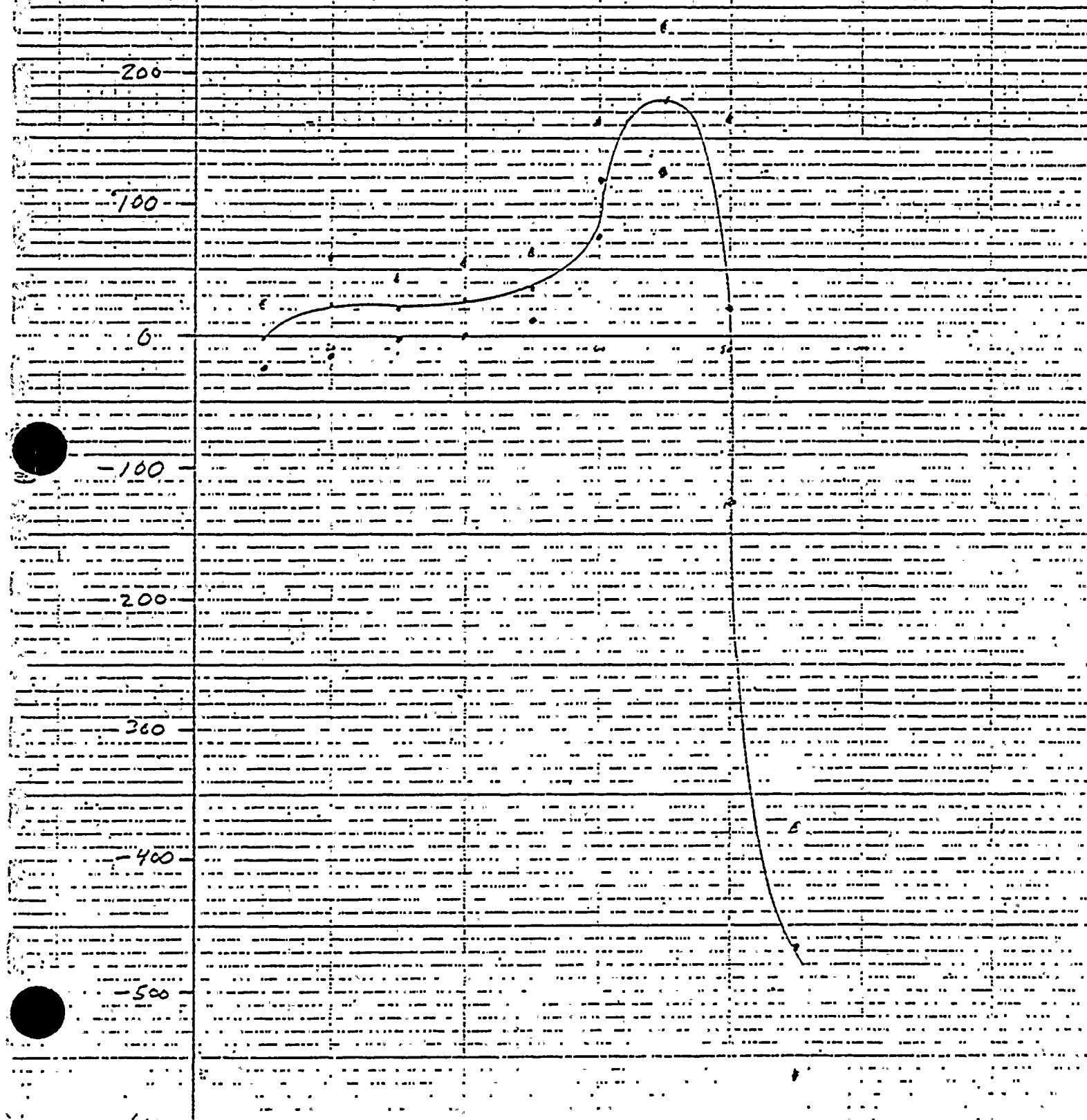
Title HYDRODYNAMIC TORQUE CURVE 12-150

Page

Calc. By C. LIVORSI

Checked By

STEM DOWNSTREAM





POSI-SEAL INTERNATIONAL, INC.

ENGINEERING CALCULATIONS

Title 12-150 STEM UP STREAM HYDRO DYNAMIC TORQUE Page \_\_\_\_\_  
Calc. By C. Liversi Checked By \_\_\_\_\_ CURVE

500

450

360

200

100

0

C OPENING

B CLOSING

ECD POINT

0 20 40 60 80 100

ANGLE OF OPENING  
DEGREES



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

Title 12"-150 (PREFERRED) HYDRODYNAMIC TORQUE CURVE Page \_\_\_\_\_  
Calc. By C. Linnert Checked By \_\_\_\_\_

500

400

300

200

100

-100

0

100

200

300

400

500

600

700

800

900

1000

1100

1200

1300

1400

1500

1600

1700

1800

1900

2000

2100

2200

2300

2400

2500

2600

2700

2800

2900

3000

3100

3200

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30600

30700

30800



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By \_\_\_\_\_

DATE: \_\_\_\_\_

Checked By \_\_\_\_\_

VALVE SIZE: 14"-150

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE:

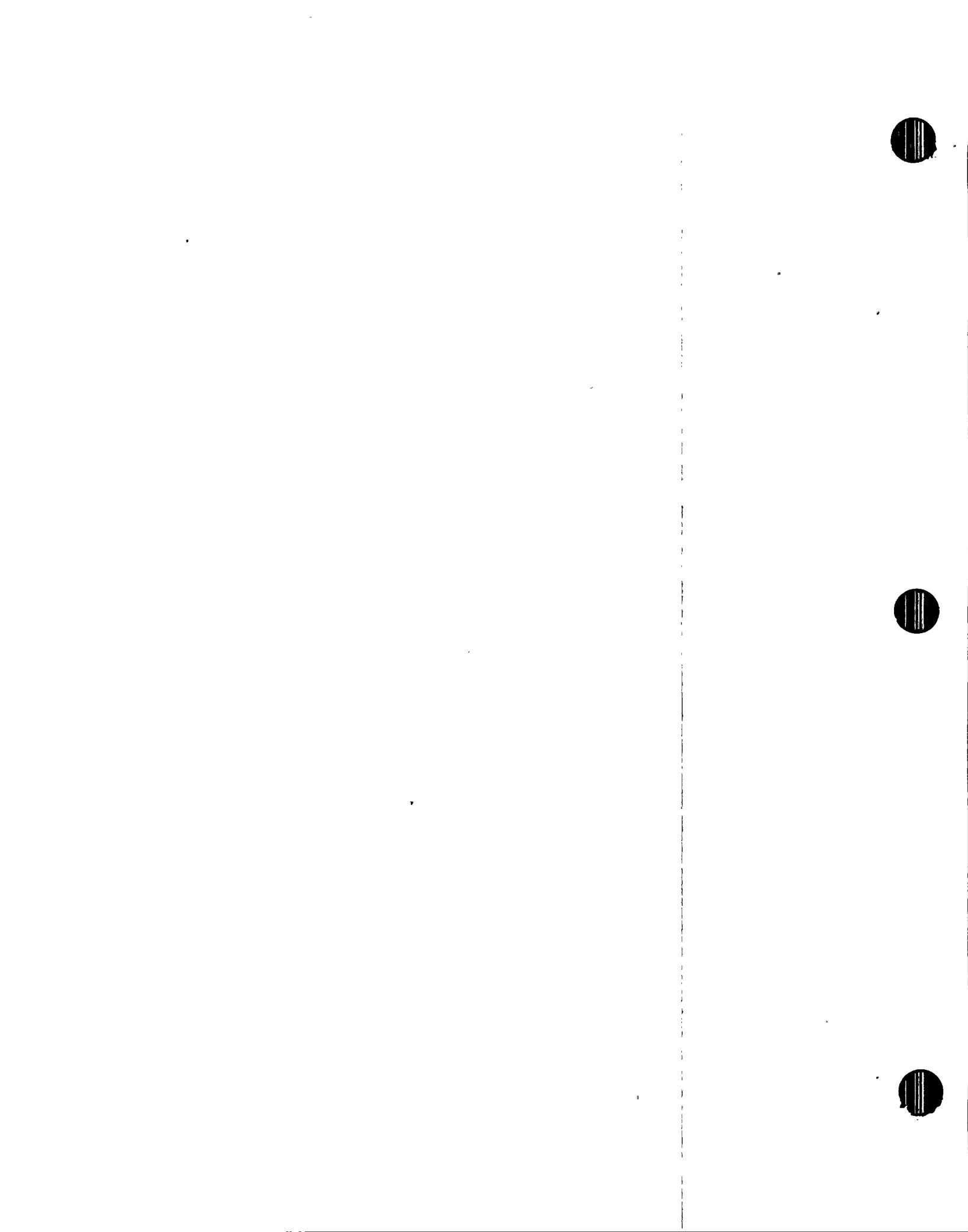
WATER TEMPERATURE (TANK): 65 °F

DISC-TYPE & DWG:

VALVE ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS + TENDING TO CLOSE - TENDING TO OPEN
OPENING	0	-	-	-
	10	49.5	525	11 - 21.5 - 675
	20	41	700	17 - 7 - 400
	30	26.5	900	34 - 20.5 - 800
	40	16	750	47 -
	50	7.2	750	104 -
	60	3	700	233 -
	70	1.5	600	400 -
	80	1	300	300 -
	90	.5	-275	-458 -
CLOSING	90	.6	-275	-458 -
	80	.7	-50	-71 -
	70	1.3	300	231 -
	60	3	500	167 -
	50	7.2	450	62.5 -
	40	15.6	200	13 -
	30	26.6	150	6 -
	20	23.6	400	17 -
	10	42.5	-300	-7 - 9 - 22 - 200 -
	0	-	-	-

PACKING TORQUE: 5 FT-LB OPENING

5 FT-LB FT-LB CLOSING



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

Title 14" 150 STEM DUVN STREAM

Page

Calc. By C. LIVORSI

Checked By

416

300

200

100

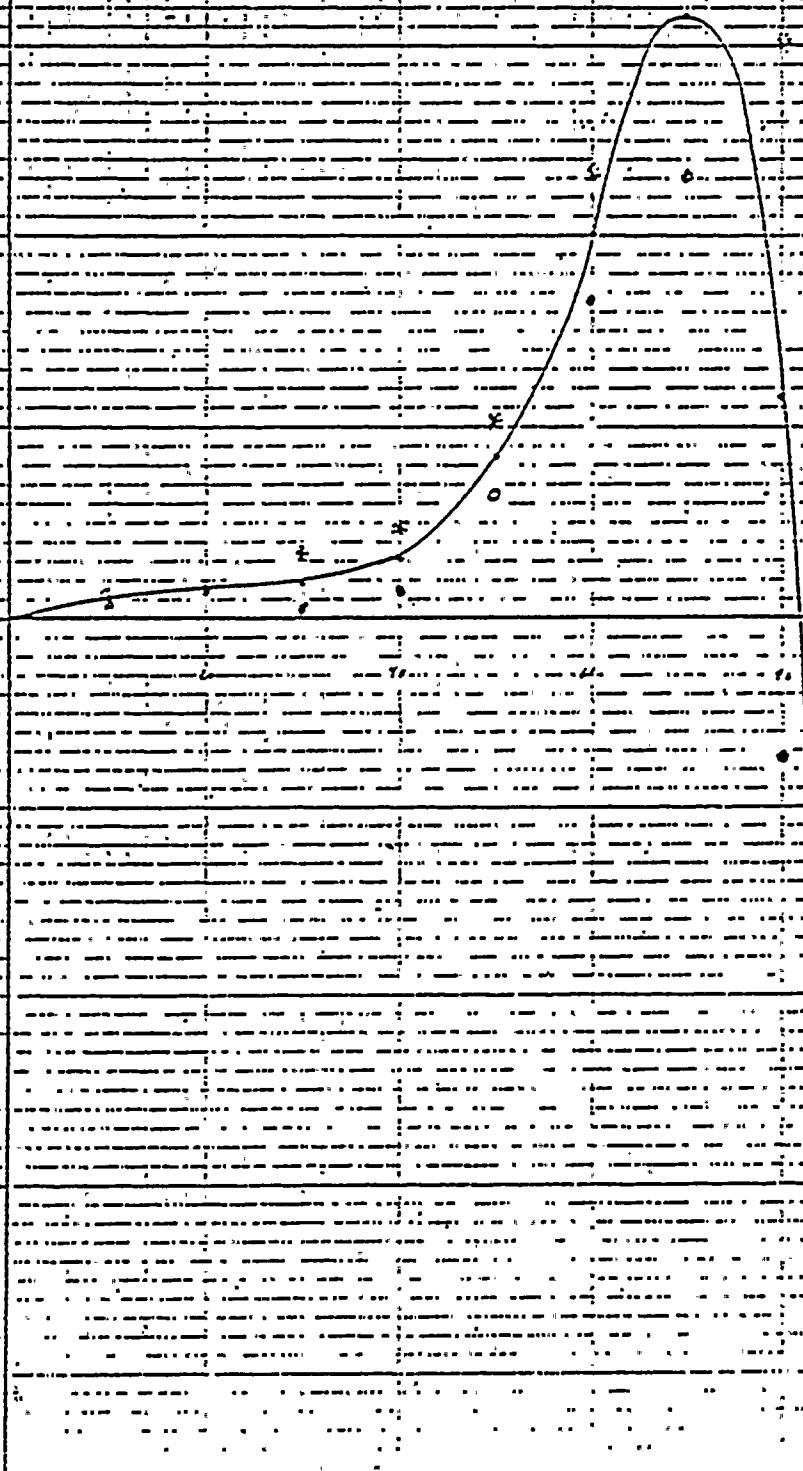
0

100

200

300

400





## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

Title TORQUE VS VALVE ANGLE

Page

Calc. By R. QANSEN

Checked By

 $10^{\circ} = 150$ 

STEM UPSTREAM  
CONTROL VALVE REGULATED

+300

+200

+100

100

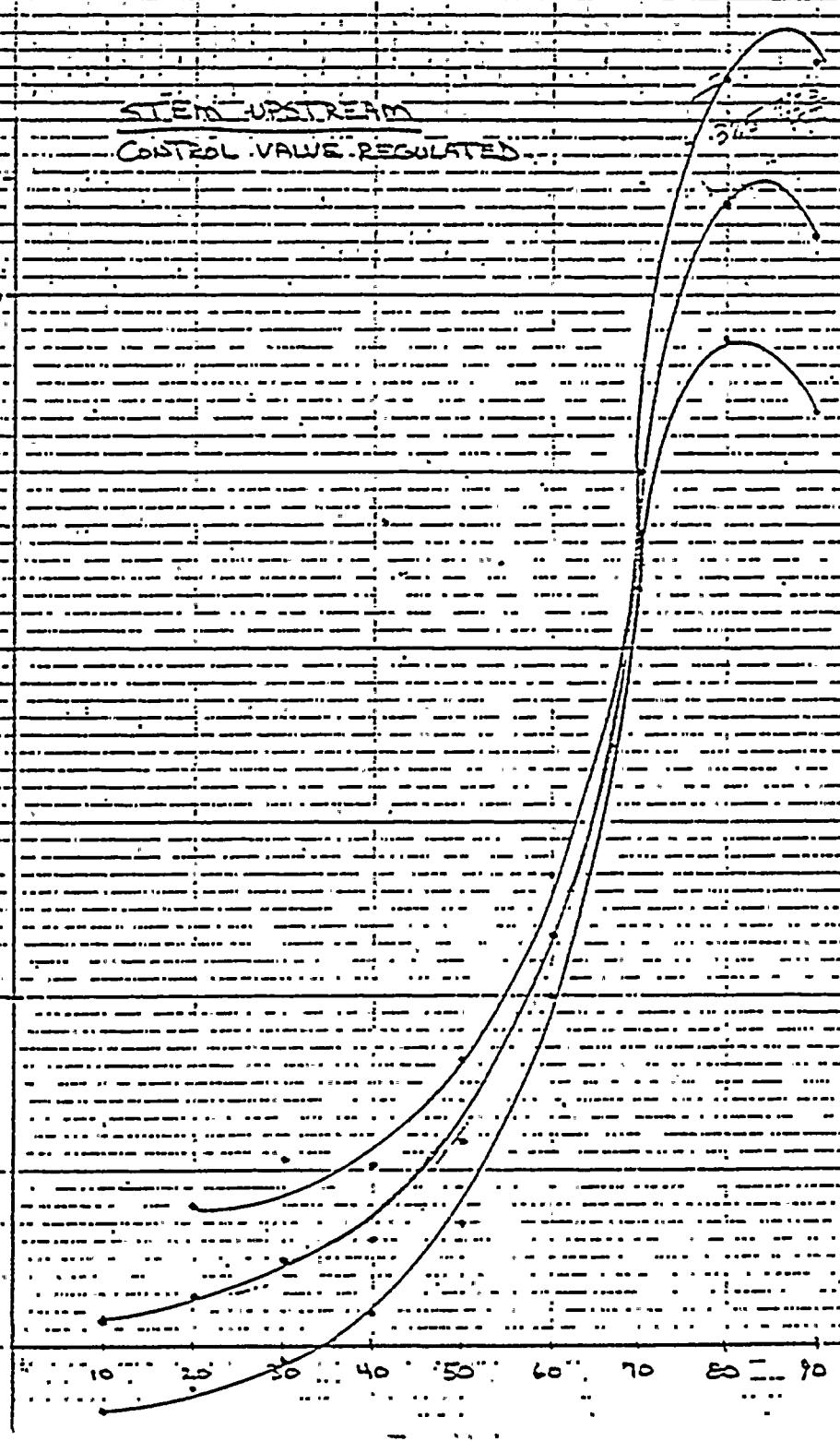
200

300

400

500

10 20 30 40 50 60 70 80 90





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title VALVE TORQUE = 10 - 150

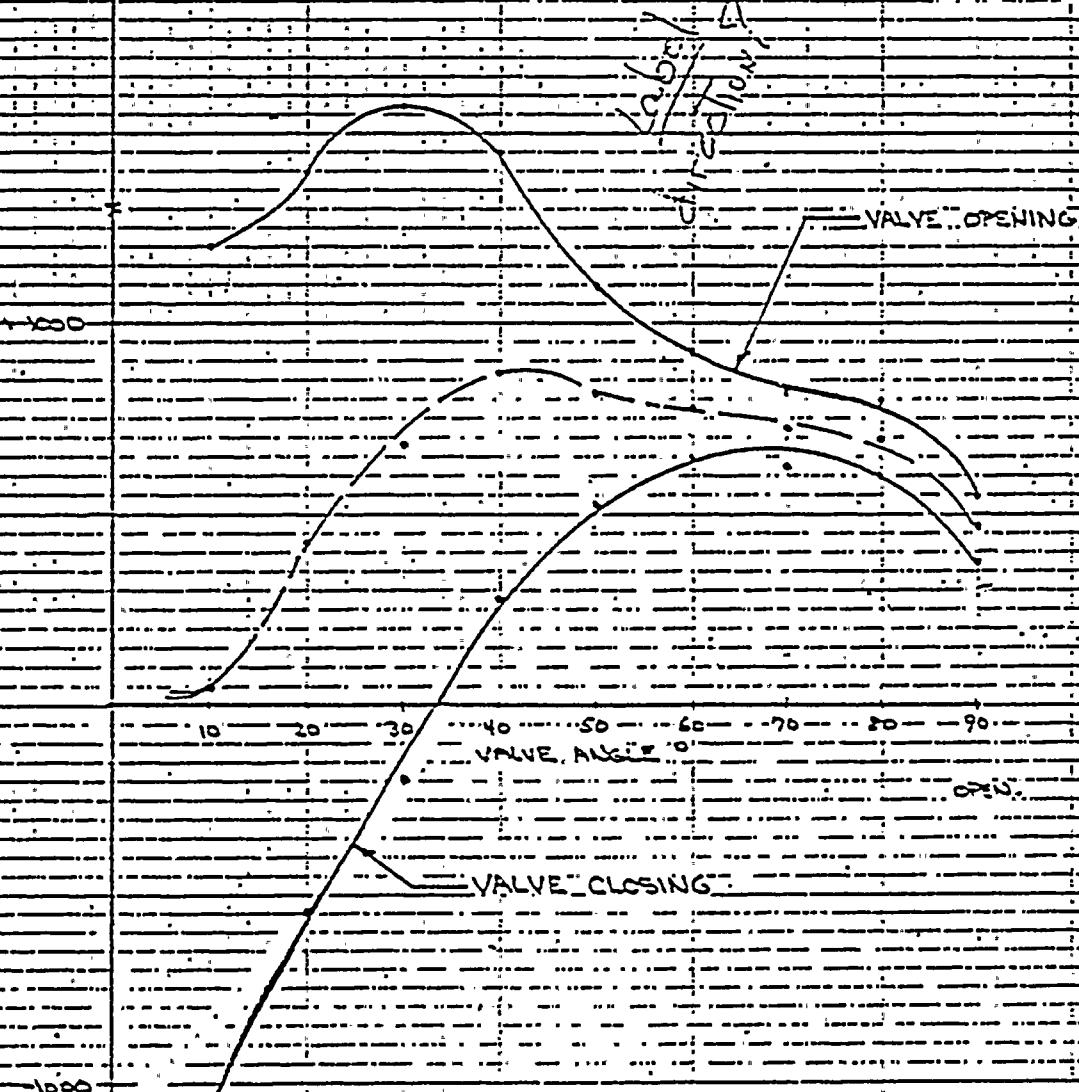
Page

Calc. By

Checked By

< CONTROL VALVE WIDE OPEN.

STEM UPSTREAM





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By C. LIVORSI DATE: 2/78 Checked By \_\_\_\_\_

VALVE SIZE: 8" 300#S



VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: STO TEFLOX

WATER TEMPERATURE (TANK): 64 °F

DISC TYPE & DWG:

VALVE ANGLE DEGREES	ΔP (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
OPENING	0	62	650	+ TENDING TO CLOSE - TENDING TO OPEN
	10	58.5	350	6.0
	20	51.5	450	8.7
	30	45	600	13.3
	40	32.5	700	21.5
	50	20	700	35
	60	18	650	36.1
	70	9.0	750	83.3
	80	6.5	750	115.4
	90	5.5	700	127.3
CLOSING	90	5.5	350	63.6
	80	6.0	550	91.7
	70	8.5	600	70.6
	60	13.0	550	42.3
	50	19.5	500	25.6
	40	30.5	450	14.7
	30	43	250	5.8
	20	52	0	0
	10	59	-150	-2.5
	0	62	550	

PACKING TORQUE: 200 IN-LB OPENING

: 200 IN-LB CLOSING



## POSI-SEAL INTERNATIONAL, INC.

## ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATIONCalc. By C. LIVORSI DATE: 2/78 Checked By \_\_\_\_\_

Page \_\_\_\_\_

VALVE SIZE: 8" 300 LB

VALVE DIRECTION:  STEM UPSTREAM /  STEM DOWNSTREAM

VALVE SEAL TYPE: S.I.D. TEFILON

WATER TEMPERATURE (TANK): 64° F

DISC TYPE: EDWAC

VALVE ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
OPENING	0	63	600	+TENDING TO CLOSE
	10	60.5	450	-
	20	51.5	550	-
	30	36	450	-
	40	22.5	350	-
	50	10.5	350	-
	60	7.0	300	-
	70	7.0	250	-
	80	5.0	0	0-TORQUE @ 78°
	90	5.0	500	-100-
CLOSING	90	4.8	550	-114.6-
	80	4.0	250	-62.5-
	70	6.0	50	-8.3-
	60	8.5	0	-G-TORQUE @ -65°-
	50	17.5	250	-14.3-
	40	30.5	250	-8.2-
	30	44	0	0
	20	50.5	0	0
	10	60.5	-250	-4.1-
	0	65	600	-

PACKING TORQUE: 200 IN-LB OPENING

: 200 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title 8"-300LB HYDRO DYNAMIC TORQUE CURVE

Page 1

Calc. By C. LIVORSI Checked By

195

150

125

100

(N-LBS)  
(PSI)

75

50

25

0

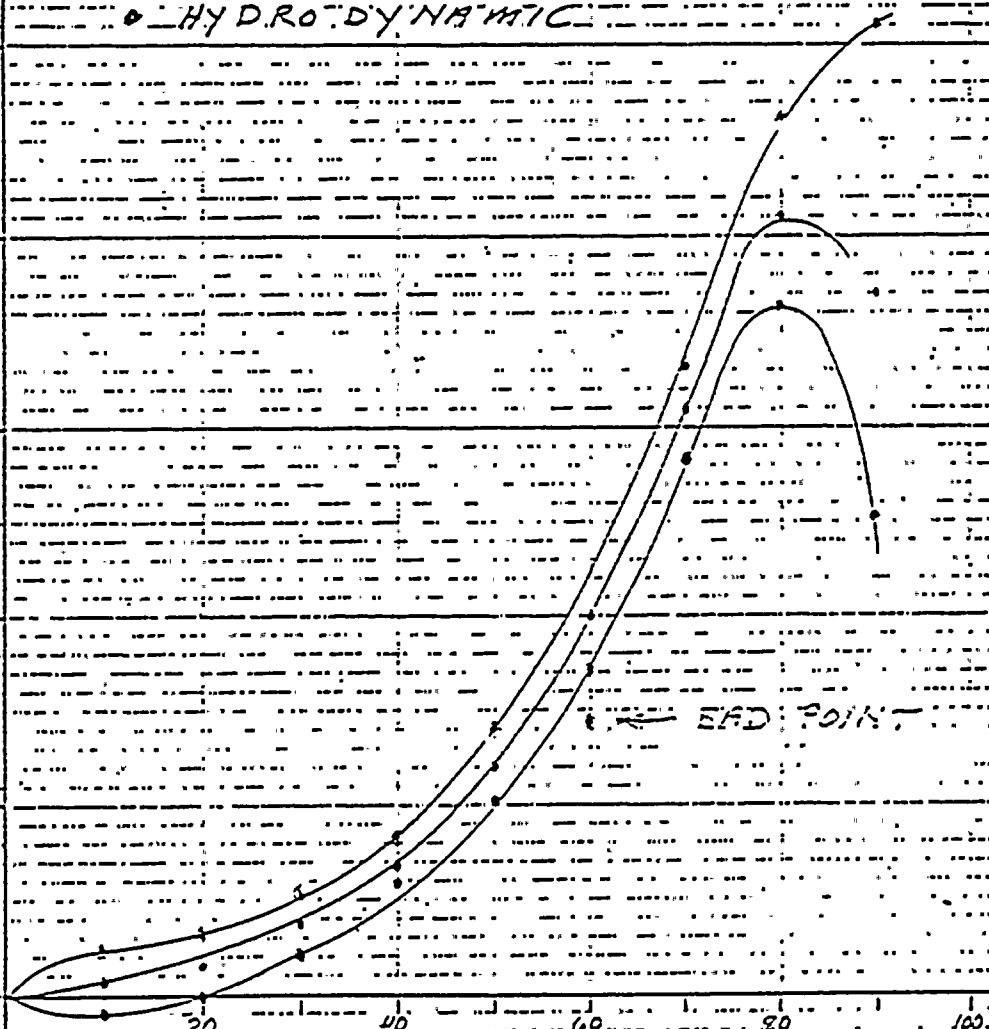
-25

OPENING

CLOSING

HYDRO DYNAMIC

END POINT



VALVE ANGLE



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title 8-300 HYDRODYNAMIC TORQUE CURVE Page \_\_\_\_\_  
Calc. By C. LIVORNEAU (UNPREFERRED) Checked By \_\_\_\_\_

75

50

25

0

1-LBS  
PSI

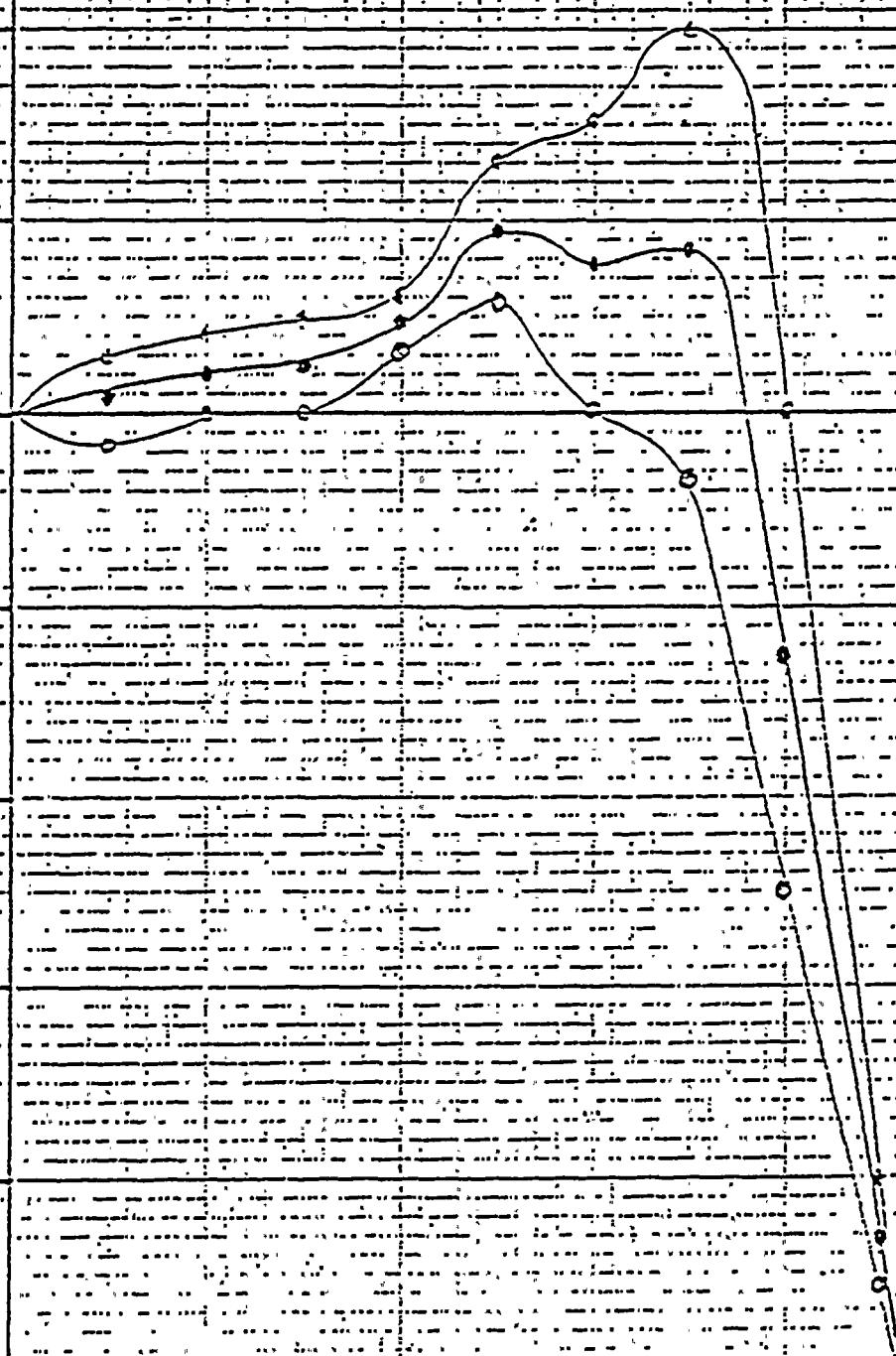
25

50

-75

-100

-125



VALVE ANGLE



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION Page  
Calc. By GANSEN DATE 8/1/77 Checked By

VALVE SIZE: 10 - 300

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL-TYPE: TEFLO/N/RUBA

WATER TEMPERATURE (TANK): 83 °F

DISC TYPE & DWG: 2

OPENING	VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE TENDING TO CLOSE IN-LB
	CLOSING				TENDING TO OPEN IN-LB
0	-	-	-	-	-
10	-	-58.5	-	-	+700
20	-	-47.5	-	-	+450
30	-	-37.5	-	-	+300
40	-	-25	-	-	+600
50	-	-10	-	-	725
60	-	-7.5	-	-	575
70	-	-4.5	-	-	200
80	-	-2.5	-	-	250
90	-	-1	-	-	500
100	-	-3	-	-	825
110	-	-3	-	-	575
120	-	-2.5	-	-	275
130	-	-1	-	-	0
140	-	-1.2	-	-	+175
150	-	-2.3	-	-	50
160	-	-37.5	-	-	300
170	-	-51	-	-	300
180	-	-57.5	-	-	600
190	-	-	-	-	-

PACKING TORQUE: 175 IN-LB OPENING

250 IN-LB CLOSING



Title HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By QANSENDATE: 7/20/77

Checked By

VALVE SIZE: 10 - 300VALVE DIRECTION: STEM UPSTREAM / STEM DOWNVALVE SEAL TYPE: TEFLON / BODAWATER TEMPERATURE (TANK): 87 °F

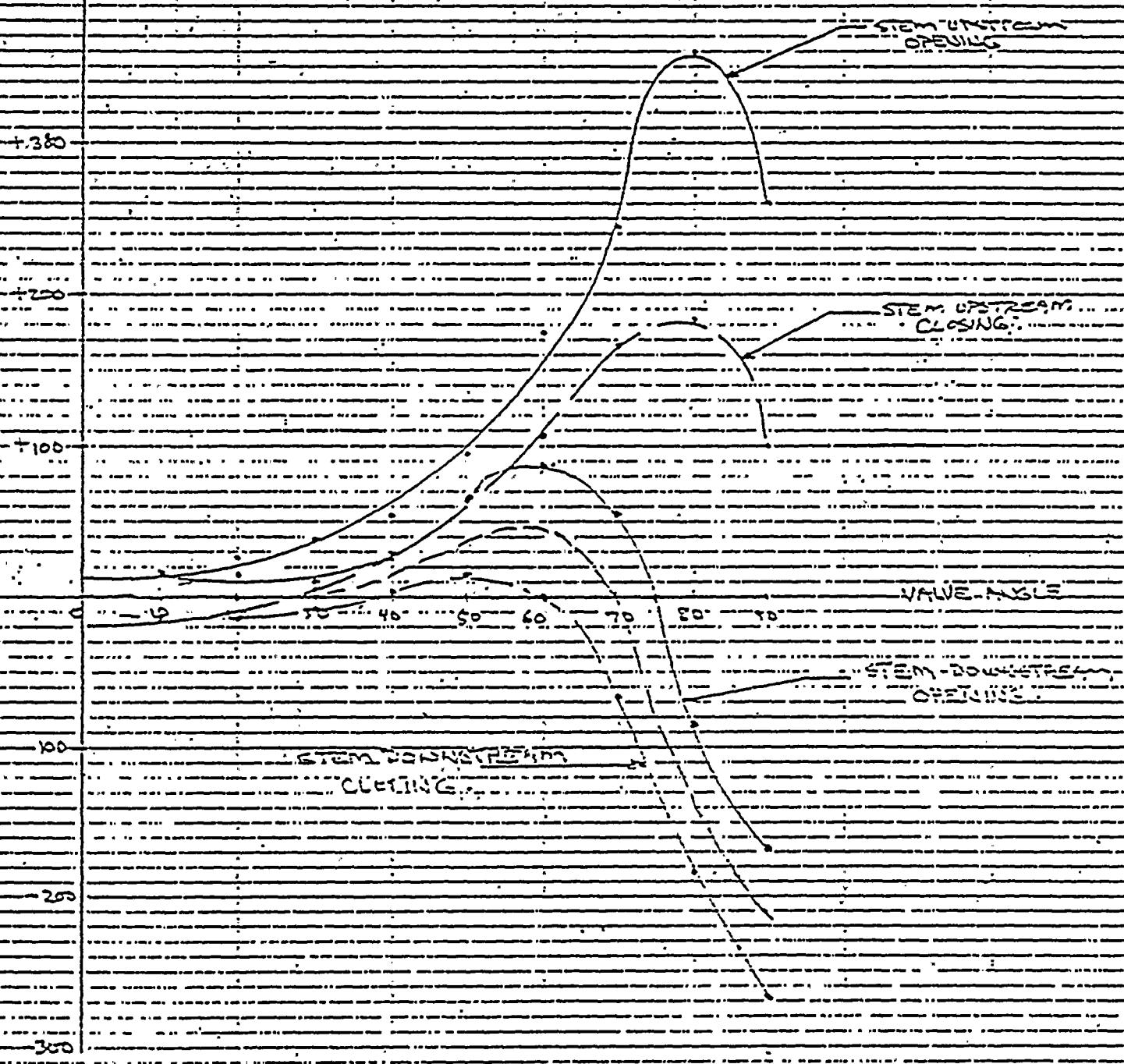
DISC TYPE &amp; Dwg.

OPENING	VALVE ANGLE DEGREES	P, PSIG	ΔP, PSI	Q, GPM	TORQUE + TENSILE TO CLOSE - TENDING TO OPEN IN-LB
	0				
	10		26		600
	20		26		770
	30		35		7350
	40		22.5		1265
	50		11		1050
	60		6		1050
	70		4.5		1100
	80		2.5		900
	90		1.5		650
			2		
	90		2.5		250
	80		3		550
	70		4.5		750
	60		7.5		850
CLOSING	50		12		750
	40		26		650
	30		12.5		750
	20		26		0
	10		55-20		550-300
	0		4		

PACKING TORQUE: 200 IN-LB OPENING250 IN-LB CLOSING



TORQUE VS. VALVE ANGLE





POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION Page  
Calc. By DANSEN DATE 3/21/77 Checked By

VALVE SIZE: 3-600

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTRE

VALVE SEAL TYPE: PLATE / BOWL

WATER TEMPERATURE (TANK): 57 °F

DISC TYPE: EDWA

	VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSIG	Q GPM	TORQUE TENDING TO CLOSE TENDING TO OPEN IN-LB
OPENING	0				
	10		-42		+60
	20		-38.5		+30
	30		-34.5		+13.5
	40		-34		+25
	50		-30.5		+40
	60		-29		+30
	70		-31.5		+0
	80		-25.5		-5
	90		-22.5		-50
CLOSING	90		-22.5		-60
	80		-25		-45
	70		-31.5		-25
	60		-38		-5
	50		-28		-10
	40		-30.5		-10
	30		-47.5		-5
	20		-46.5		-10
	10		-47.5		-125
	0				

PACKING TORQUE: 10 IN-LB OPENING  
5 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By Conan DATE 3/4/77 Checked By

VALVE SIZE : 3" - 600

VALVE DIRECTION (STEM UPSTREAM) / STEM DOWNSTRE

VALVE SEAL TYPE : Teflon/Rubber

WATER TEMPERATURE (TANK) : +68 °F

DISC TYPE & DWG

OPENING	VALVE	P <sub>1</sub>	A <sub>P</sub>	Q	TORQUE
	ANGLE DEGREES	UPSTREAM PSIG	PSI	GPM	+TENDING TO CLOSE -TENDING TO OPEN IN-LB
	0				
	10		54		+75
	20		52		+60
	30		43.5		+75
	40		40.5		+75
	50		43.5		+145
	60		37.5		+120
	70		31.5		+145
	80		26		+160
	90		23		+145
	100		23		+140
	110		26.5		+125
	120		31		+115
	130		35		+100
	140		43.5		+75
	150		38.5		+45
	160		41.5		0
	170		43		0
	180		44		-55
	190		47		
CLOSING					
	180				
	170				
	160				
	150				
	140				
	130				
	120				
	110				
	100				
	90				
	80				
	70				
	60				
	50				
	40				
	30				
	20				
	10				
	0				

PACKING TORQUE : 40 IN-LB OPENING

5 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title: HYDRODYNAMIC TORQUE DETERMINATION Page

Calc. By Dansen DATE: 11/10/77 Checked By

VALVE SIZE: 4" 600

VALVE DIRECTION: (STEM UPSTREAM) / STEM DOWNSTREAM

VALVE SEAL TYPE: TEFON / EPR

WATER TEMPERATURE (TANK): 60° F

DISC TYPE & DWG:

VALVE ANGLE DEGREES	DP PSI.G	Q GPM	TORQUE IN-LB TENDING TO CLOSE	TORQUE IN-LB TENDING TO OPEN
0	0	0	0	0
10	.49	6.5	+275	-
20	.35	13.5	+275	-
30	.34	22.5	+250	-
40	.23.5	35	+175	-
50	.26.5	50	+175	-
60	.26	65	+250	-
70	.22	80	+225	-
80	.19	95	+250	-
90	.16.5	110	+150	-
100	.17	125	+150	-
110	.21.5	140	+125	-
120	.27.5	150	+150	-
130	.35.5	165	+75	-
140	.42.5	180	+150	-
150	.39	195	+125	-
160	.48.25	210	250	-250
170	.26.5	225	250	-250
180	0	240	0	0

PACKING TORQUE: 15 IN-LB OPENING

5 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

HYDRODYNAMIC TORQUE DETERMINATION

Calc. By GÄUSEN Date 11/3/77 Checked By \_\_\_\_\_

Page \_\_\_\_\_

VALVE SIZE : 4-600

VALVE DIRECTION : STEM UPSTREAM / SYSTEM DOWNSTREAM

VALVE SEAL TYPE : TEFLOL / EPR

WATER TEMPERATURE (TANK) : 68 °F

DISC TYPE & DWG :

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE IN-LB
0				
10		43		75
20		40.5		25
30		37		50
40		44.5		50
50		39		50
60		31		25
70		23.5		25
80		19		75
90		13.5		125
100				
110				
120				
130				
140				
150				
160				
170				
180				
CLOSING				
0				
10				
20				
30				
40				
50				
60				
70				
80				
90				
100				
110				
120				
130				
140				
150				
160				
170				
180				

PACKING TORQUE : 250 IN-LB OPENING

: 250 IN-LB CLOSING



## Title HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By Douglas DATE: 18/7/77 Checked By \_\_\_\_\_

VALVE SIZE: 6-600

VALVE DIRECTION: OPEN UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: Teflon / Buna

WATER TEMPERATURE (TANK): 83 °F

DISC TYPE &amp; DWG:

	VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE TENDING TO CLOSE IN-LB
OPENING	0		X		X
	10		44		+250
	20		33		+150
	30		27.5		+250
	40		25		+450
	50		19.5		+450
	60		20.5		+450
	70		15		+250 +667
	80		10.5/8.5		-250
	90		7.5		650
CLOSING	90		7.5		-850
	80		19.0		-500
	70		18.5		-200
	60		26		-50
	50		28		-50
	40		33		0
	30		34		-275
	20		32.5		-350
	10		39		-350
	0		41		X

PACKING TORQUE: 175 IN-LB OPENING

225 IN-LB CLOSING



FRICTION COEFFICIENTS  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION Page \_\_\_\_\_

Calc. By Danen DATE: 12/19/77 Checked By \_\_\_\_\_

VALVE SIZE 6-600

VALVE DIRECTION STEM UPSTREAM / STEM TO ANGLE

VALVE SEAL TYPE TEFON / BWA

WATER TEMPERATURE (TANK) 85 °F

DISC TYPE EDWG 20°

VALVE ANGLE DEGREES	P <sub>1</sub> UPSTREAM PSI	ΔP PSI	Q GPM	TORQUE IN-LB
0	30.5	25	15	+
10	33.1	28.5	15	+
20	24	55.5	15	+
30	25	49.5	15	+
40	26.5	49.5	15	+
50	20	32.5	15	+
60	19.6	24.5	15	+
70	19.2	19.0	15	+
80	14.8	14.8	15	+
90	14.8	14.8	15	+
80	19.3	18.8	15	+
70	24.2	24.4	15	+
60	20.5	31.5	15	+
50	24.5	43.5	15	+
40	34.5	50.5	15	+
30	34.5	55.5	15	+
20	38.5	58	15	+
10	34.8	60.5	15	+
0	0	87	15	+

PACKING TORQUE IN-LBS IN-LB OPENING

IN-LB CLOSING



## HYDRODYNAMIC TORQUE V.S. ANGLE

Page

Calc. By J CORY 8/23/77 Checked By

80

6" = 600

PREFERRED DIRECTION

70

60

50

40

35.3

30

25

20

15.1

10

5

0

ANGLE FACTOR

0 0

10 8

20 20

30 40

40 70

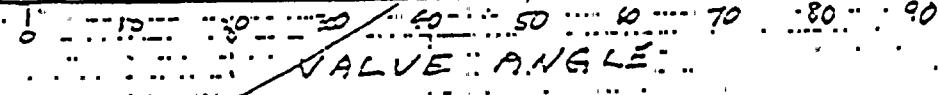
50 11.0

60 17.0

70 34.0

80 46.0

90 47.0





## ENGINEERING CALCULATIONS

Job No. HYDRODYNAMIC TORQUE V.S. ANGLE

Page

Calc. By J. CORY 8/23/77 Checked By

6° - 60°

NON-PREFERRED DIRECTION

150

+40

T30

+20

+10

0

-10

-20

-30

-40

-50

-60

-70

-80

-90

0 10 20 30 40 50 60 70 80 90

ANGLE FACTOR

0 0

10 -3

20 -3

30 0

40 -7

50 12

60 12

70 4

80 -22

90 -22



## ENGINEERING CALCULATIONS

Title: HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By: L. L. Cooksill DATE: Checked By \_\_\_\_\_

VALVE SIZE: 8" 600#

VALVE DIRECTION:  STEM UPSTREAM  STEM DOWNSTREAM

VALVE SEAL TYPE: URATHANE

WATER TEMPERATURE (TANK): 69° F

DISC TYPE: EDWG

VALVE ANGLE DEGREES	Δ P (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
0	0	-4600	-	
10	5.0	500	-10-	
20	11.5	250	-22.7-	
30	17.5	-300	-26.1-	
40	23.0	350	-34.8-	
50	27.5	325	-34.2-	
60	31.7	200	-35.7-	
70	36.5	-125	-19.2-	72° TORQUE WENT
80	5.0	-125	-25	NEG
90	6.0	-300	-50	
90	6.0	-600	-100	
80	5.0	-400	-80	
70	7.0	-250	-35.7	
60	11.2	-700	-8.9	
50	18.5	-10	0	
40	23.5	-700	4.3	
30	31.0	100	3.2	
20	39	-200	5.4	
10	5.7	-250	-4.4	
0	0	-1100	-	

PACKING TORQUE: 150 IN-LB OPENING

150 IN-LB CLOSING



## ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATIONCalc. By C. LIOVSKI

DATE:

Checked By

Page

VALVE SIZE: 8-600VALVE DIRECTION:  STEM UPSTREAM /  STEM DOWNVALVE SEAL TYPE: URATHANEWATER TEMPERATURE (TANK): 71.9

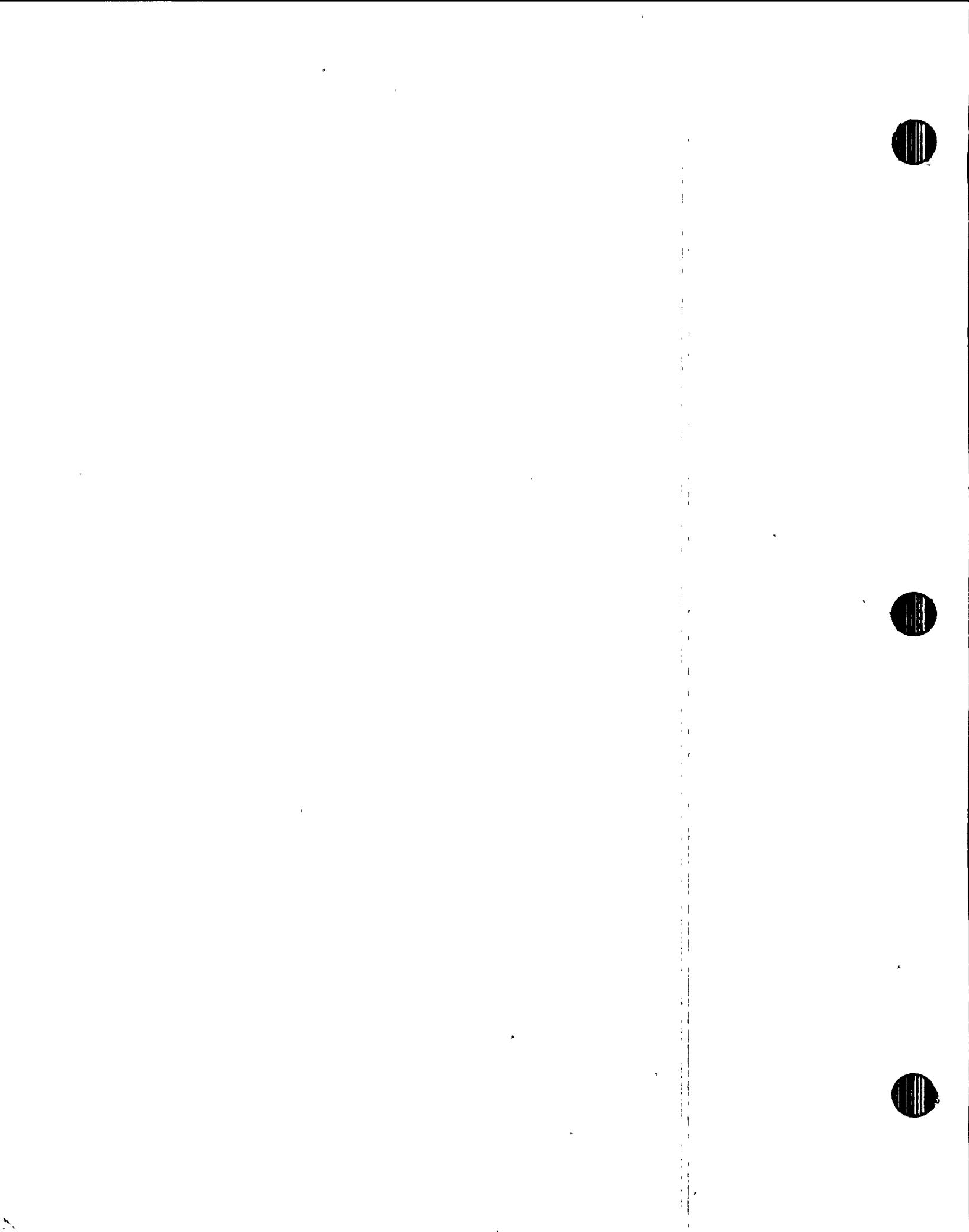
DISC TYPE &amp; DWG:

VALVE ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
0	67	7800		TENDING TO CLOSE
10	50.5	400		
20	10	300	19.8	TENDING TO OPEN
30	5	250	50	
40	1.8	1400	42	
50	0.9	600	66.7	
60	0.6	300	83.3	
70	0.2	180	42.5	
80	0.0	100	13.3	
90	-0.6	300	65	
100	-1.5	0	0	
110	-2.2	-200	50	
120	-3.5	-325	59.4	
130	-5.8	-525	45.6	
140	-14.5	-300	26.4	
150	-9.0	-100	14.1	
160	-19.0	-115	6.1	
170	-19.0	-0	0	
180	-49.0	-350	7.4	
190	-62	-1800		

OPENING

CLOSING

PACKING TORQUE: 150 IN-LB OPENING150 IN-LB CLOSING



8"-600LB

HYDRODYNAMIC TORQUE CURVE (NON-PREP DIRECTION)

Calc. By:

C. LIVORE

Checked By:

Page

40

20

0

IN-LBS

PSI

20

40

60

80

100

120

HYDRODYNAMIC  
TORQUE

0

20

40

60

80

100

VALVE ANGLE (DEGREES)



8-6001-B

ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE CURVE (PERF. DIRECTION)

Page

Calc. By

C. LIPORSI

Checked By

140

120

100

80

60

40

20

0

-20

HYDRODYNAMIC  
TORQUE

20 40 60 80 100

VALVE ANGLE  
(DEGREES)



## ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION Page  
 Calc. By DALESEN DATE: 8/3/77 Checked By

Control Valve - Regel valve

VALVE SIZE: 10" 600

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: TEFILON/ISUNA

WATER TEMPERATURE (TANK): 84°F

DISC TYPE & DWG: 2

VALVE ANGLE DEGREES	P, PSIG	ΔP, PSI	Q, GPM	TORQUE TENDING TO CLOSE IN-LB	TORQUE TENDING TO OPEN IN-LB
0					
-10		47.385		900	
-20		32.255		1200	
-30		28.825		1500	
-40		26.744		1800	1750
-50		14.944		2150	1550
-60		16.598		2450	1350
-70		7.3		2400	
-80		5.2		1200	
-90		4.4		800	
-95.25		4.8		0	
-80		4.4		200	
-70		5.9		450	
-60		8.8		550	
-50		53.0		600	
-40		20.8		650	
-30		33		450	
-20		40.4		50	
-10		39		550	
0		9		2	

PACKING TORQUE: 35.0 IN-LB OPENING

45.0 IN-LB CLOSING



## ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Calc. By

Duncan

DATE: 8/5/77

Page

Checked By

Control valve regulated

VALVE SIZE: 10" 600

VALVE DIRECTION: OPEN UPSTREAM STEM DOWN

VALVE SEAL TYPE: TEFILON / BUNP

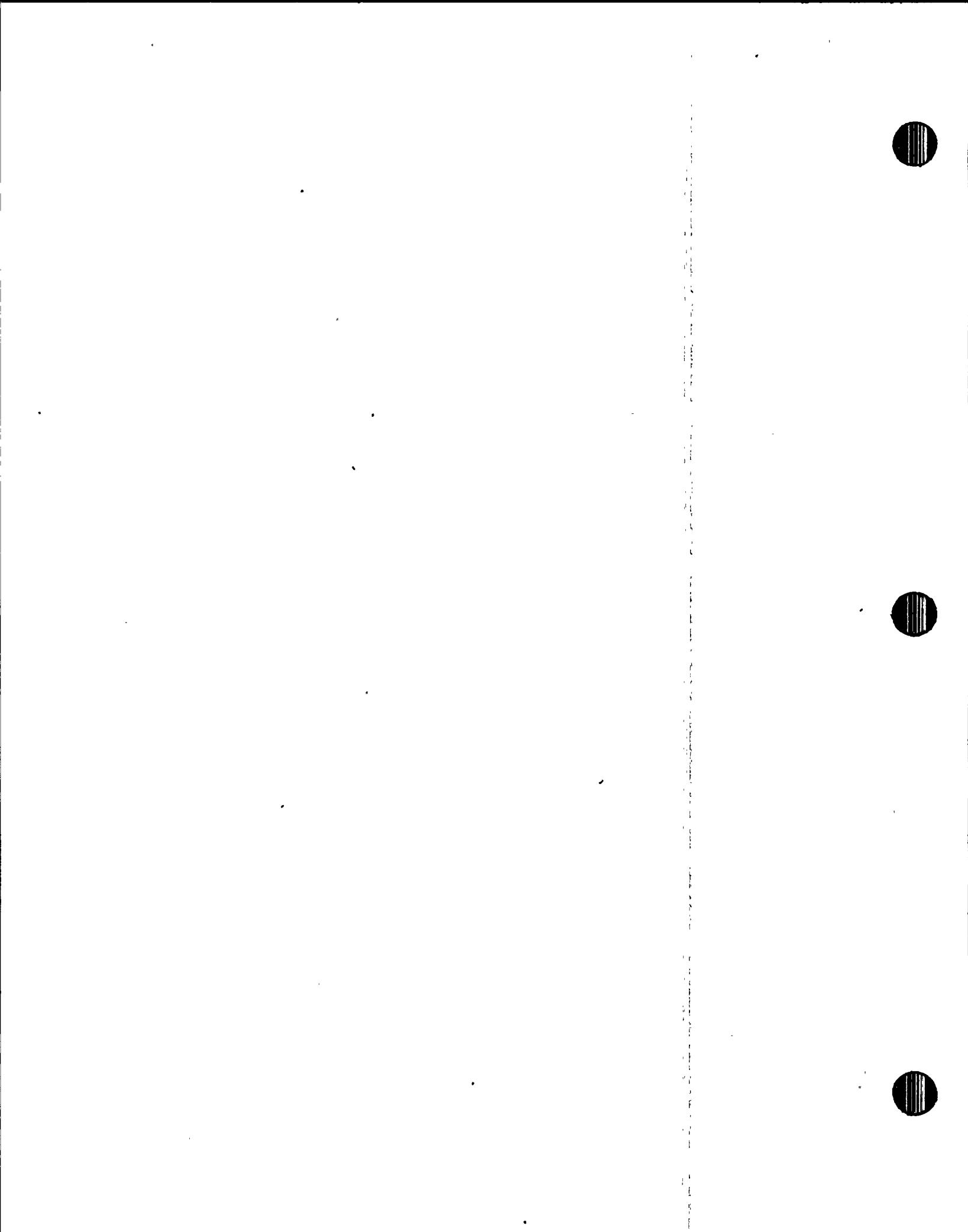
WATER TEMPERATURE (TANK): 88° OF

DISC TYPE &amp; Dwg: 2

VALVE ANGLE DEGREES	P, UPSTREAM PSIG	ΔP PSI	Q GPM	TORQUE + TENDING TO CLOSE - TENDING TO OPEN IN-LB
OPENING	0	EX		X
	10	46		HEE
	20	31.5		+ 900
	30	27.5		+ 900
	40	24.5		2000
	50	14.0		+ 100
	60	9.1		- 950 - 800
	70	5.8		+ 600 - 400
	80	4.3	4.7	- 350 - 250
	90	4.1		250
CLOSING	90	4.7		250
	80	4.2		250
	70	8.4		- 550
	60	9.6		- 450
	50	14.4		300
	40	26.5		- 250
	30	27.5		- 400
	20	32		- 750
	10	37		800
	0	EX		X

PACKING-TORQUE: 50 IN-LB OPENING

150 IN-LB CLOSING



## HYDRODYNAMIC TORQUE DETERMINATION

Title HYDRODYNAMIC TORQUE DETERMINATION

Page

Calc. By

Date: 8/5/77

Checked By

Control valve valve open

VALVE SIZE: 10"-600

VALVE DIRECTION: OPEN UPSTREAM / STEM DOWN

VALVE SEAL TYPE: TEFON/BONF

WATER TEMPERATURE (TANK): 88°F

DISC TYPE EDG 2

VALVE ANGLE DEGREES	P, PSI	ΔP, PSI	Q, GPM	TORQUE TENDING TO CLOSE IN-LB
OPENING 0		X		
10		57		40,500
20		48.5		950
30		39		225
40		25.5		250
50		14.5		900
60		9.4		900
70		6.5		250
80		4.3		0,25
90		4.6		300
CLOSING 90		X		1250
80		4.2		800
70		6.4		550
60		7.8		500
50		14.0		325
40		24.5		325
30		37.2		575
20		49.0		900
10		57.5		1035
0		X		450

PACKING TORQUE: 850 IN-LB OPENING

450 IN-LB CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION Page 1  
Calc. By C. Livolesi DATE: 9-1-78 Checked By \_\_\_\_\_

VALVE SIZE: 10" 1500 LB

VALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTREAM

VALVE SEAL TYPE: METAL

WATER TEMPERATURE (TANK): 77 °F

DISC TYPE & DWG:

OPENING ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE ( <del>IN-LBS</del> ) FT-LBS	$\frac{FT}{IN-LBS}$ PSI	COMENTS	
				TENDING TO CLOSE	TENDING TO OPEN
0					
10	59.5	190	3.2		
20	54.5	195	3.6		
30	40.5	205	5.1		
40	24.5	205	8.4		
50	17.5	190	10.9		
60	12.0	175	14.6		
70	9.5	165	17.4		
80	8.0	160	20.0		
90	7.5	145	19.3		
90	8.0	-35	-4.4		
80	7.5	-20	-2.7		
70	8.0	-5	-0.6		
60	8.5	-5	-0.6		
50	11.5	-5	-0.4		
40	17.5	-10	-0.6		
30	31.0	-50	-1.6		
20	44.5	-105	-2.4		
10	52.5	-210	-4.0		
0					

PACKING TORQUE: 70 FT-LBS ~~IN-LB~~ OPENING

70 FT-LBS ~~IN-LB~~ CLOSING



## ENGINEERING CALCULATIONS

Title HYDRODYNAMIC TORQUE DETERMINATION

Page \_\_\_\_\_

Calc. By C. LIVORSIDATE: 9-1-78

Checked By \_\_\_\_\_

VALVE SIZE: 14" 1500 LBVALVE DIRECTION: STEM UPSTREAM / STEM DOWNSTVALVE SEAL TYPE: METALWATER TEMPERATURE (TANK): 77°FDISC TYPE & DWG:

VALVE ANGLE DEGREES	$\Delta P$ (PSIG)	TORQUE (IN-LBS)	IN-LBS PSI	COMENTS
OPENING	0	0	0	TENDING TO CLOSE
	10	59.5	150	2.6
	20	48.5	190	3.9
	30	39.0	200	5.1
	40	25.5	170	6.7
	50	16.5	130	7.9
	60	12.5	90	7.2
	70	9.0	50	5.5
	80	7.5	25	3.3
	90	6.8	15	2.2
CLOSING	90	7.0	-115	-16.4
	80	7.0	-115	-16.4
	70	7.2	-95	-13.2
	60	8.0	-90	-11.3
	50	11.5	-70	-6.1
	40	19.5	-65	3.3
	30	32.0	-70	2.2
	20	45.0	-100	2.2
	10	54.0	-125	2.3
	0			

PACKING TORQUE: 70 FT-LBS IN-LBS OPENING70 FT-LBS IN-LBS CLOSING



POSI-SEAL INTERNATIONAL, INC.  
ENGINEERING CALCULATIONS

14" 1500 LB HYDRODYNAMIC TORQUE CURVE Page

Calc. By C. LIVOREV

Checked By

PERFERED

25

20

15

10

FL-LBS

PSI of ΔP

5

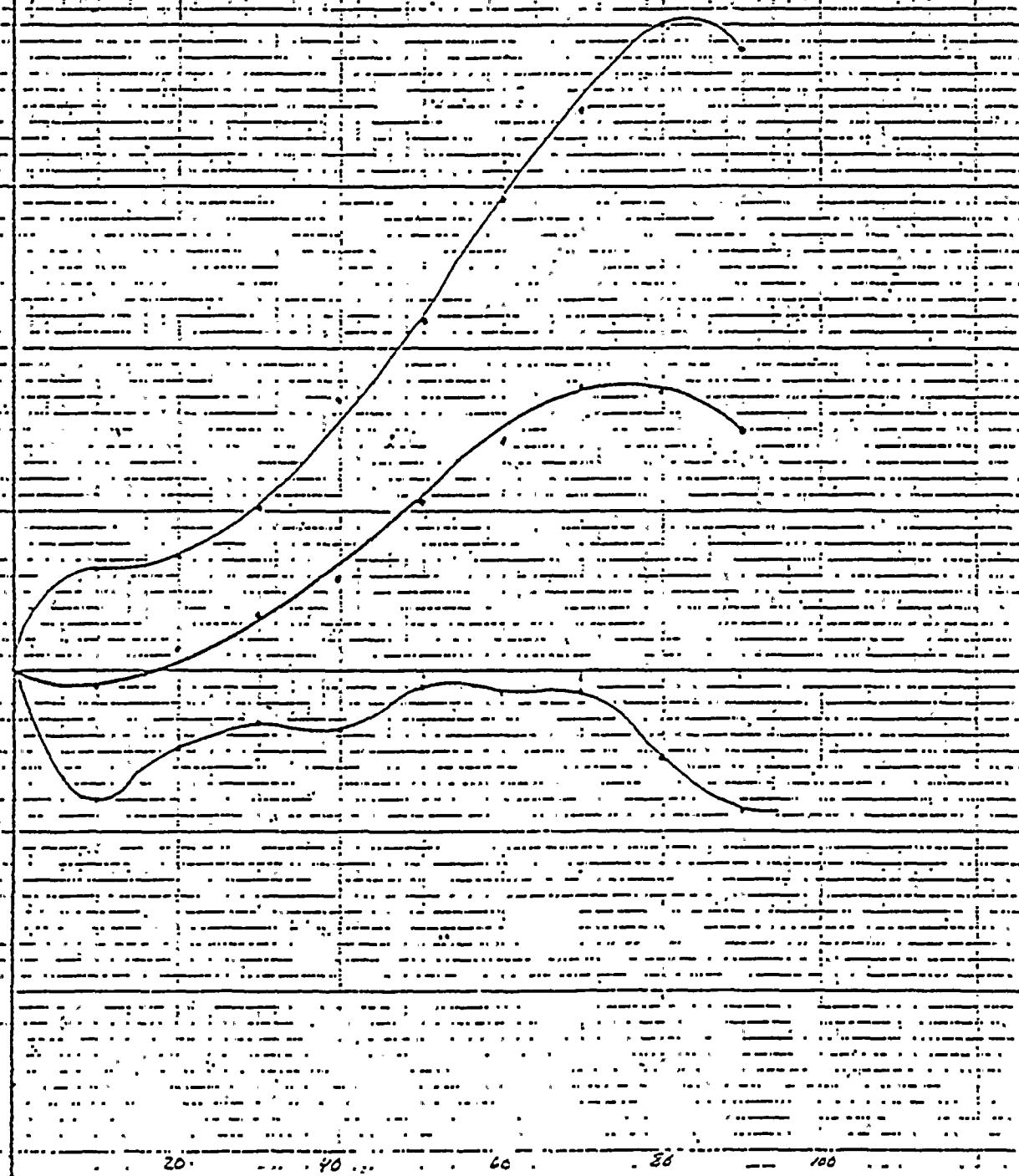
0

5

10

20 40 60 80 100

VALVE ANGLE  
DEGREES OPEN





POISEUL INTEGRATIONAL, INC.  
ENGINEERING CALCULATIONS

14-1500 LBS HYDRODYNAMIC TORQUE CURVE

Page

By

C. LIVORSI

Checked By

IS

NON PREFERRED

10

5

12-135

0

XT of ΔP

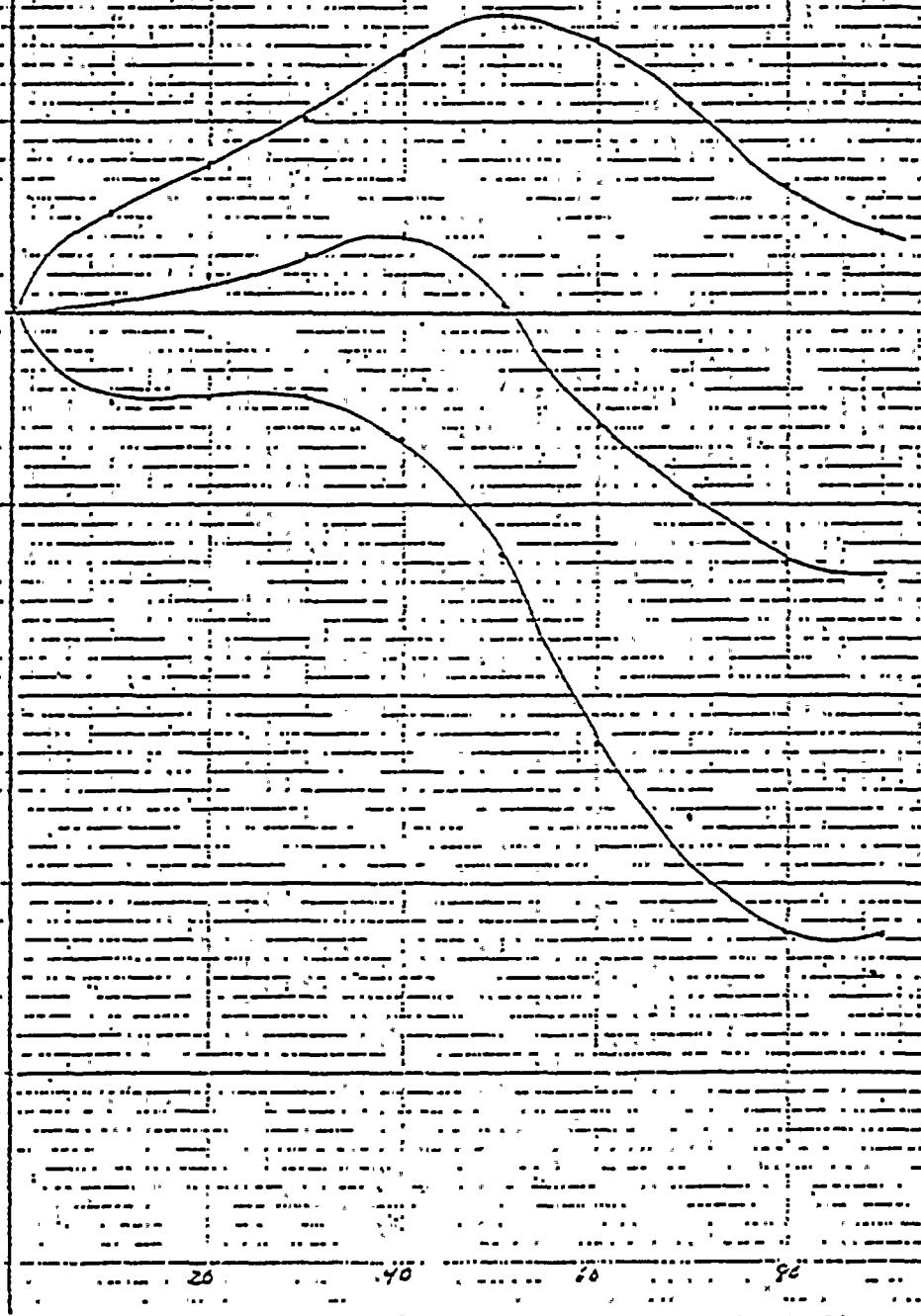
5

10

15

20

25



VALVE ANGLE  
DEGREES OPEN





## TECHNICAL BULLETIN NO. 1A

### Operating torque values and Actuator sizing

JUNE 82

#### TORQUE VALUES TO OPEN AND SHUT

The Posi-Seal Trunnion Valve is a low torque valve which normally reaches its highest torque when opening. This torque value will vary with the seat material and stem packing selected in addition to the maximum operating differential pressure ( $\Delta P$ ) across the valve.

Torque values to open and shut for standard Posi-Seal Trunnion Valves are listed in Tables 1, 2 and 3, and are denoted as  $T_1$ ,  $T_2$ , and  $T_3$ .

$T_1$  and  $T_2$  torque values are due to the stem packing and seat material selected and are added together to determine preload torque.

The static pressure torque factor  $T_3$  is the static pressure torque per  $\text{PSI} \Delta P$ . This factor ( $T_3$ ) is multiplied by the maximum operating  $\Delta P$  or maximum line pressure to obtain the torque value due to pressure.

To obtain the maximum torque to open or shut the  $T_1$ ,  $T_2$ , and  $T_3$   $\Delta P$  values are simply added together.

#### EXAMPLE:

A. Requirement — What is the maximum opening torque of a 12" Class 150 valve with teflon chevron packing, a teflon seal ring with rubber back-up ring and a maximum  $\Delta P$  of 200 PSI.

B. Solution — From Table 1

$$T_1 = (B) = 70 \text{ in. lbs.}$$

$$T_2 = (G) = 986 \text{ in. lbs.}$$

$$T_3 = 10.10 \text{ in. lbs. per } \text{PSI} \Delta P = 10.10 \times 200 = 2020 \text{ in. lbs.}$$

$$\text{Total opening torque} = T_1 + T_2 + (T_3 \times \text{PSI} \Delta P) = 70 + 986 + (10.10 \times 200) = 3076 \text{ in. lbs.}$$

Although the valve opening torque is normally the highest operating torque used in actuator sizing, it is often necessary with flowing liquids to check for total hydrodynamic torque. Refer to Section II for data on calculating total hydrodynamic torque.

# Posi-Seal Technical Bulletin No. 1A

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TABLE I  
CLASS 150 STANDARD RATING

VALVE SIZE	PRELOAD TORQUE = $T_1 + T_2$								STATIC PRESSURE TORQUE PER PSI $T_3$	
	$T_1$			$T_2$						
	A	B	C	E	F	G	H	J	316 M.S.	REXNORD
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
3"	302	28	227	122	73	61	244	280	0.24	.16
4"	338	31	254	218	131	109	436	501	0.50	.33
6"	454	42	340	510	306	255	1020	1173	1.56	1.04
8"	529	49	397	902	541	451	1804	2074	3.23	2.15
10"	680	63	510	1398	839	699	2796	3215	6.44	4.29
12"	756	70	567	1972	1183	986	3944	4535	10.10	6.73
14"	832	77	624	2424	1454	1212	4848	5575	13.66	9.11
16"	907	84	680	3164	1898	1582	6328	7277	19.44	12.96
18"	1058	98	794	3994	2396	1997	7988	9186	28.64	19.09
20"	1210	112	907	4914	2948	2457	9828	11302	40.28	26.85
24"	1512	140	1134	7564	4538	3782	15128	17397	77.48	51.65
30"	1814	168	1361	11982	7189	5991	23964	27558	147.28	98.19
36"	2268	210	1701	17426	10456	8713	34852	40080	267.76	178.51
42"	2419	672	1814	23795	14277	11897	47590	54728	390.00	.....
48"	2722	756	2041	30864	18518	15432	61728	70987	569.00	.....
54"	2722	756	2041	39849	23909	19924	79698	91653	734.70	.....
60"	3024	840	2268	49280	29568	24640	98561	113345	1010	.....
66"	3326	924	2495	59937	35962	29969	119875	137856	1351	.....
72"	3629	1008	2722	71355	42813	35677	142709	164115	1754	.....

CLASS 150 150PSI RATING

VALVE SIZE	PRELOAD = $T_1 + T_2$								STATIC PRESSURE TORQUE PER PSI $T_3$	
	$T_1$			$T_2$						
	A	B	C	E	F	G	H	J	316 M.S.	REXNORD
24"	1210	112	907	7194	4316	3597	14388	16546	58.96	39.31
30"	1512	140	1134	12038	7223	6019	24076	27687	123.32	82.21
36"	1663	154	1247	17420	10452	8710	34840	40066	196.28	130.85
42"	1966	546	1474	23846	14308	11923	47693	54847	317.50	.....
48"	2268	630	1701	31069	18642	15535	62139	71460	477.30	.....
54"	2268	630	1701	39849	23909	19924	79698	91653	612.12	.....
60"	2268	630	1701	49484	29691	24742	98969	113814	760.30	.....
66"	3024	840	2268	59937	35962	29969	119875	137856	1228	.....
72"	3024	840	2268	71661	42997	35830	143322	164820	1468	.....

Valve torque (opening) =  $T_1 + T_2 + (T_3 \times \text{PSI} \Delta P)$

Valve torque (closing, on-off service) =  $T_1 + T_2 + (.5T_3 \times \text{PSI} \Delta P)$

Valve torque (closing, modulating service) =  $T_1 + T_2 + (T_3 \times \text{PSI} \Delta P)$

When the operating  $\Delta P$  used for actuator selection is less than the maximum line pressure, contact the factory for sizing torque.

NOTES:

- (A) Asbestos jam packing
- (B) Teflon Chevron packing
- (C) Graphite jam packing

$T_2$  (E) Urethane seal ring with rubber back-up ring, Metal seal ring with and without rubber back-up ring, Kel-F seal ring without rubber back-up ring

- (F) Teflon seal ring with Teflon back-up ring, Tefzel seal ring with rubber back-up ring
- (G) Teflon seal ring with rubber back-up ring
- (H) Metal seal ring with Teflon insert and rubber back-up ring
- (J) Metal seal ring with urethane, Tefzel, or Kel-F insert and rubber back-up ring

# Posi-Seal Technical Bulletin No. 1A

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TABLE 2  
CLASS 300 STD. RATING

VALVE SIZE	PRELOAD TORQUE = $T_1 + T_2$								STATIC PRESSURE TORQUE PER PSI $T_3$	
	$T_1$			$T_2$						
	A	B	C	E	F	G	H	J	316 M.S.	REXNORD
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
3"	302	28	227	122	73	61	244	280	0.24	.16
4"	338	31	254	218	131	109	436	501	0.50	.33
6"	454	42	340	510	306	255	1020	1173	1.56	1.04
8"	756	70	567	750	450	375	1500	1725	3.84	2.56
10"	907	84	680	1242	745	621	2484	2857	7.64	5.09
12"	1058	98	794	1722	1063	886	3544	4076	12.70	8.47
14"	1210	112	907	2160	1296	1080	4321	4968	17.71	11.81
16"	1361	126	1021	3164	1898	1582	6328	7277	29.16	19.44
18"	1512	140	1134	3602	2161	1801	7204	8285	36.90	24.60
20"	1814	168	1361	4534	2720	2267	9068	10428	55.74	37.16
24"	2117	196	1588	7564	4538	3782	15128	17397	108.46	72.31
30"	2722	252	2041	10764	6458	5382	21528	24757	198.45	132.30
36"	3024	280	2268	16278	9767	8139	32556	37439	333.46	222.31
42"	3175	294	2381	23402	14041	11701	46804	53825	503.30	.....
48"	4234	392	3175	30383	18230	15192	60766	69881	871.40	.....

$$\text{Valve torque (opening)} = T_1 + T_2 + (T_3 \times \text{PSI} \Delta P)$$

$$\text{Valve torque (closing, on-off service)} = T_1 + T_2 + (.5T_3 \times \text{PSI} \Delta P)$$

$$\text{Valve torque (closing, modulating service)} = T_1 + T_2 + (T_3 \times \text{PSI} \Delta P)$$

When the operating  $\Delta P$  used for actuator selection is less than the maximum line pressure, contact the factory for sizing torque.

#### NOTES:

T<sub>1</sub> (A) Asbestos jam packing

(B) Teflon Chevron packing

(C) Graphite jam packing

T<sub>2</sub> (E) Urethane seal ring with rubber back-up ring, Metal seal ring with and without rubber back-up ring, Kel-F seal ring without rubber back-up ring

(F) Teflon seal ring with Teflon back-up ring, Tefzel seal ring with rubber back-up ring

(G) Teflon seal ring with rubber back-up ring

(H) Metal seal ring with Teflon insert and rubber back-up ring

(J) Metal seal ring with urethane, Tefzel, or Kel-F insert and rubber back-up ring

TABLE 3  
TORQUE VALUES (In. Lbs.)  
Class 600 Posi-Seal Trunnion Valves

VALVE SIZE	PRELOAD TORQUE ( $T_1 + T_2$ )										STATIC PRESSURE TORQUE PER PSI $T_3$	
	$T_1$					$T_2$						
	A	B	C	D	E	F	G	H	J	316 M.S.	REXNORD	
3"	342	AVAILABLE ON APPLICATION	257	95	120	72	NOT AVAILABLE IN CLASS 600	AVAILABLE ON APPLICATION	276	0.27	.18	
4"	454		340	126	202	121			465	0.63	.42	
6"	529		397	147	496	298			1141	1.77	1.18	
8"	907	AVAILABLE ON APPLICATION	680	252	770	462	NOT AVAILABLE IN CLASS 600	AVAILABLE ON APPLICATION	1771	4.73	3.15	
10"	1058		794	294	1234	750			2838	8.85	5.9	
12"	1361		1021	378	1724	1034			3965	15.89	10.59	
14"	1512	AVAILABLE ON APPLICATION	1134	420	2078	1247	NOT AVAILABLE IN CLASS 600	AVAILABLE ON APPLICATION	4779	21.29	14.19	
16"	1814		1361	504	2698	1619			6205	33.17	22.11	
18"	2117		1588	588	3532	2119			8124	50.64	33.76	
20"	2419	AVAILABLE ON APPLICATION	1814	672	4238	2543	NOT AVAILABLE IN CLASS 600	AVAILABLE ON APPLICATION	9747	69.4	46.27	
24"	2722		2041	756	6422	3853			14770	118.4	78.93	

$$\text{Valve torque (opening)} = T_1 + T_2 + (T_3 \times \text{PSI} \Delta P)$$

$$\text{Valve torque (closing, on-off service)} = T_1 + T_2 + (.5T_3 \times \text{PSI} \Delta P)$$

$$\text{Valve torque (closing, modulating service)} = T_1 + T_2 + (T_3 \times \text{PSI} \Delta P)$$

When the operating  $\Delta P$  used for actuator selection is less than the maximum line pressure, contact the factory for sizing torque.

#### NOTES:

- $T_1$  (A) Asbestos jam packing  
 (B) Teflon Chevron packing — available on application  
 (C) Graphite jam packing  
 (D) Teflon jam packing
- $T_2$  (E) Metal seal ring with and without rubber back-up ring, Kel-F ring without rubber back-up ring  
 (F) Tefzel seal ring with rubber back-up ring  
 (G) Not available on Class 600  
 (H) Metal seal ring with Teflon insert and rubber back-up ring — available on application  
 (J) Metal seal ring with Tefzel, or Kel-F insert and rubber back-up ring (urethane insert available on application)

## II. TOTAL VALVE OPERATING HYDRODYNAMIC TORQUE

As previously stated the valve opening torque is normally the highest operating torque used for actuator sizing and selection. However, when flowing liquids, it is often necessary to calculate the total valve operating hydrodynamic torque.

The location of the maximum valve operating torque (total hydrodynamic torque) is a result of the overall system operating parameters in addition to the particular valve disc hydrodynamic torque characteristics.

When the ratio of thru valve  $\Delta P$  to total system  $\Delta P$  is high, generally above 25 percent, the maximum valve operating hydrodynamic torque will occur at or about the 70° to 80° disc open position. As this ratio decreases, the maximum valve operating hydrodynamic torque will shift towards the 0° shut position.

To allow for system operating variables it is recommended that the maximum valve operating hydrodynamic torque ( $TH_T$ ) be calculated at both the 20° and 80° disc open position.

The total valve operating hydrodynamic torque ( $TH_T$ ) is the summation of three torque components. These components are: stem packing torque ( $T_1$ ), stem bearing friction torque (static pressure torque per  $PSI\Delta P$ ) and the disc hydrodynamic lift and drag torque. Torque values  $T_1$  and  $T_3$  can be found in Tables 1 thru 3.

Extensive flow testing has shown that the disc hydrodynamic lift and drag torque values are dependent upon the direction of flow entering the valve. With liquid flow entering the valve from the stem side, with the seal retaining downstream, the disc hydrodynamic lift and drag torque value ( $T_4$ ) is positive to the full open position acting to return the disc to the shut position. Liquid flow entering the valve from the opposite direction, seal retaining ring upstream, results in a torque value that remains positive, acting to return the disc to the shut position, until about the 70° to 80° open position. At this point the torque value becomes negative acting to move the disc to the full open position. With liquid flow in this direction the disc hydrodynamic lift and drag torque values are designated as  $T_5$ . Also, test results have shown that flowing liquids in this direction results in a positive  $T_5$  value that is lower than the corresponding  $T_4$  value with flow in opposite direction.

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By utilizing torque values  $T_1$  and  $T_3$  along with the applicable disc hydrodynamic lift and drag torque values  $T_4$  or  $T_5$  listed in Tables 4 thru 9, the total valve operating hydrodynamic torque  $TH_T$  can be calculated as follows:

## RETAINING RING DOWNSTREAM

$$TH_T = T_1 + (T_3 \Delta P) + (T_4 \Delta P) G_f$$

## RETAINING RING UPSTREAM

$$TH_T = T_1 + (T_3 \Delta P) + (T_5 \Delta P) G_f$$

$TH_T$  = Total valve operating hydrodynamic torque, in. lbs.

$T_1$  = Packing torque, in. lbs. Tables 1, 2, and 3.

$T_3$  = Stem bearing friction torque (static pressure torque per  $\text{PSI} \Delta P$ ), in. lbs. Tables 1, 2, and 3.

$T_4$  = Disc hydrodynamic lift and drag torque, in. lbs. Flow into valve with retaining ring downstream.

$T_5$  = Disc hydrodynamic lift and drag torque, in. lbs. Flow into valve with retaining ring upstream.

$\Delta P$  = Differential pressure across valve, PSI.

$G_f$  = Specific gravity of liquid at flowing conditions.

$G_f$  = Density of liquid at flowing conditions  
Density of water at standard conditions

## EXAMPLE:

A. Requirement — What is the total valve hydrodynamic torque of a 12" CLASS 150 Valve with teflon chevron packing, flowing water into the valve from the stem side (retaining ring downstream) with a calculated  $\Delta P$  of 10 PSI at the 70° disc open position.

## B. Solution —

$$TH_T = T_1 + (T_3 \Delta P) + (T_4 \Delta P) G_f$$

$$TH_T = 70 + [10.10 (10)] \div [692 (10)] 1.0$$

$$TH_T = 7091 \text{ in. lbs.}$$

Where —

$$T_1 = 70 \text{ in. lbs.}$$

$$T_3 = 10.10 \text{ in. lbs.}$$

$$T_4 = 692$$

$$G_f = 1.0$$

## NOTE:

When in doubt about the maximum total valve hydrodynamic torque for a specific application, contact Posi-Seal factory for assistance.

TABLE 4

## CLASS 150 STD RATING

Seal Retaining Ring Downstream  
Disc Hydrodynamic Lift & Drag Torque -  $T_4$

VALVE SIZE	T <sub>4</sub> VS. OPEN POSITION								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
3"	0	0	0	0	1	2	5	6	5
4"	0	0	1	1	3	6	12	16	13
6"	1	2	4	8	13	27	51	68	56
8"	4	10	16	30	49	100	185	247	204
10"	6	16	26	49	79	161	300	399	330
12"	15	38	60	114	182	372	692	920	761
14"	23	59	94	177	283	579	1075	1430	1182
16"	41	102	164	307	492	1005	1876	2482	2052
18"	64	162	259	486	778	1590	2953	3927	3245
20"	99	248	397	746	1193	2437	4526	6019	4974
24"	214	536	858	1610	2576	5259	9768	12988	10734
30"	462	1156	1850	3469	5551	11334	21049	27988	23131
36"	1884	4710	7537	14132	22611	46164	85734	113998	94213
42"	2281	5704	9127	17114	27383	55908	103829	138058	114098
48"	3265	8164	13063	24494	39191	80016	148602	197592	163299
54"	7388	18471	29554	55414	88662	181020	336180	447008	369428
60"	11165	27913	44661	83740	133984	273552	508026	675506	558270
66"	14942	37355	59768	112066	179306	366084	679972	904005	747112
72"	22995	57488	91981	172465	275945	563388	1046293	1391225	1149773
CLASS 150 150 PSI RATING									
24"	255	637	1020	1913	3061	6251	11609	15437	12758
30"	857	2144	3431	6433	10293	21016	39030	51897	42890
36"	1792	4480	7168	13441	21505	43907	81542	108424	89607
42"	3202	8007	12811	24021	38434	78469	145729	193772	160142
48"	5412	13530	21648	40591	64946	132598	246254	327437	270609
54"	7336	18341	29346	55025	88040	179749	333820	443871	366835
60"	14428	36072	57715	108216	173146	353506	656512	872945	721442
66"	14942	37355	59768	112066	179306	366084	679872	904005	747112
72"	30124	75310	120496	225931	361490	738044	1370653	1822516	1506212

1. T<sub>4</sub> values = in. lbs. per PSIΔP.

2. All T<sub>4</sub> values are positive acting to shut valve.

3. 0 T<sub>4</sub> values  $\leq$  < 1.

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TABLE 5

## CLASS 150 STD. RATING

Seal Retaining Ring Upstream  
Disc Hydrodynamic Lift & Drag Torque -  $T_s$

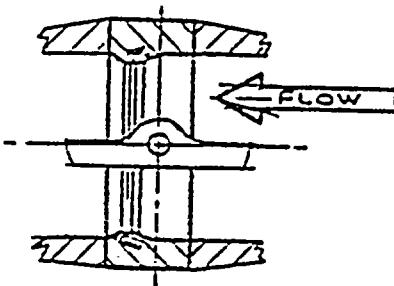
VALVE SIZE	T <sub>s</sub> VS. DISC OPEN POSITION								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
3"	0	0	0	0	0	1	1	0	-5
4"	0	0	0	0	1	3	4	0	-13
6"	0	1	2	2	5	13	19	-1	-56
8"	2	4	8	10	18	46	69	-4	-204
10"	3	6	13	16	.29	75	112	-6	-330
12"	7	15	30	38	68	175	258	-15	-761
14"	11	23	47	59	106	271	402	-23	-118
16"	20	41	82	102	184	471	697	-41	-2052
18"	32	64	129	162	292	746	1103	-64	-3245
20"	49	99	198	248	447	1144	1691	-99	-4974
24"	107	214	429	536	966	2468	3649	-214	-10734
30"	231	462	925	1156	2081	5320	7864	-462	-23131
36"	942	1884	3768	4710	8479	21669	32032	-1884	-94213
42"	1140	2281	4563	5704	10268	26242	38793	-2281	-114098
48"	1632	3265	6531	8164	14696	37558	55521	-3265	-163299
54"	3694	7388	14777	18471	33248	84968	125605	-7388	-369428
60"	5583	11165	22330	27913	50244	128402	189812	-11165	-558270
66"	7471	14942	29884	37355	67240	171835	254018	-14942	-747112
72"	11497	22995	45990	57488	103479	264447	390922	-22995	-1149773
CLASS 150 150 PSI RATING									
24"	127	255	510	637	1148	2934	4337	-255	-12758
30"	428	857	1715	2144	3860	9864	14582	-857	-42890
36"	896	1792	3584	4480	8064	20609	30466	-1792	-89607
42"	1601	3202	6405	8007	14412	36832	54448	-3202	-160142
48"	2706	5412	10824	13530	24354	62240	92007	-5412	-270609
54"	3668	7336	14673	18341	33015	84372	124724	-7336	-366835
60"	7214	14428	28857	36072	64929	165931	245290	-14428	-721442
66"	7471	14942	29884	37355	67240	171835	254018	-14942	-747112
72"	15062	30124	60248	75310	135559	346428	512112	-30124	-1506212

1.  $T_s$  values = in. lbs. per PSI $\Delta P$ .
2. Except as noted,  $T_s$  values are positive acting to shut valve.

3. Negative (-)  $T_s$  values act to move the disc to the full open (90°) position.
4. 0  $T_s$  values  $\cong < 1$ .

TABLE 6

## CLASS 300 STD RATING

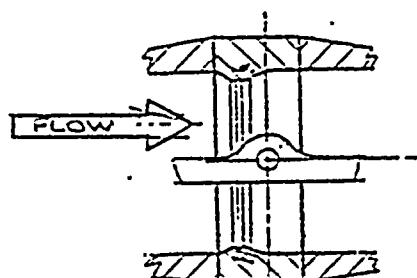
Seal Retaining Ring Downstream  
Disc Hydrodynamic Lift & Drag Torque -  $T_4$ 

VALVE SIZE	$T_4$ VS. DISC OPEN POSITION								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
3"	0	0	0	0	1	2	5	6	5
4"	0	0	1	1	3	6	12	16	13
6"	1	2	4	8	13	27	51	68	56
8"	1	4	7	11	21	34	57	81	68
10"	3	9	17	27	51	81	136	192	162
12"	7	21	39	60	113	179	298	422	355
14"	9	29	54	84	158	250	416	590	495
16"	12	37	68	105	198	313	520	737	620
18"	28	86	158	244	460	726	1208	1711	1438
20"	30	92	169	261	493	778	1294	1833	1540
24"	41	125	229	355	668	1054	1754	2485	2088
30"	143	429	788	1218	2292	3618	6019	8526	7165
36"	287	861	1579	2441	4596	7253	12065	17092	14363
42"	686	2058	3773	5381	10976	17321	28812	40817	34300
48"	429	1287	2359	3646	6864	10832	18018	25526	21451

1.  $T_4$  values = in. lbs. per PSI $\Delta P$ .
2. All  $T_4$  values are positive acting to shut valve.
3. 0  $T_4$  values  $\geq < 1$ .

TABLE 7

## CLASS 300 STD RATING



Seal Retaining Ring Upstream  
Disc Hydrodynamic Lift & Drag Torque -  $T_s$

VALVE SIZE	$T_s$ VS. DISC OPEN POSITION								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
.....	.....	.....	.....	.....	.....	.....	.....	.....	.....
3"	0	0	0	0	0	1	1	0	-5
4"	0	0	0	0	1	3	4	0	-13
6"	0	1	2	2	5	13	19	-1	-56
8"	0	1	2	6	8	10	4	-22	-68
10"	1	3	6	14	21	24	11	-53	-162
12"	3	7	14	31	46	53	24	-117	-355
14"	4	9	19	44	64	74	34	-163	-495
16"	6	12	24	55	80	93	43	-204	-620
18"	14	28	57	129	187	215	100	-474	-1438
20"	15	30	61	138	200	231	107	-508	-1540
24"	20	41	83	187	271	313	146	-689	-2088
30"	71	143	286	644	931	1074	501	-2364	-7165
36"	143	287	574	1292	1867	2154	1005	-4739	-14363
42"	343	686	1372	3087	4459	5145	2401	-11319	-34300
48"	214	429	858	1930	2788	3217	1501	-7078	-21451

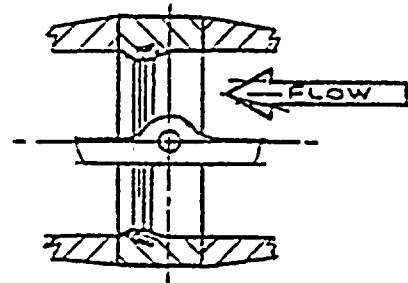
1.  $T_s$  values = in. lbs. per PSI $\Delta P$ .
2. Except as noted,  $T_s$  values are positive acting to shut valve.
3. Minus  $T_s$  values are negative and act to move the disc to the full open (90°) position.
4. 0  $T_s$  values  $\cong < 1$ .

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TABLE 8

## CLASS 600 STD RATING



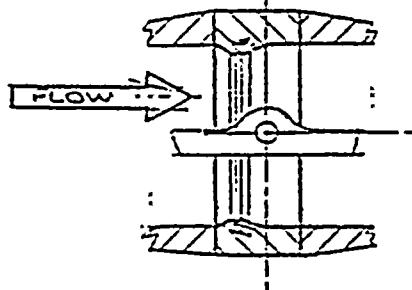
Seal Retaining Ring Downstream  
Disc Hydrodynamic Lift & Drag Torque -  $T_4$

VALVE SIZE	$T_4$ VS. DISC OPEN POSITION								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
3"	0	0	0	0	0	0	0	0	0
4"	0	0	0	0	0	0	0	0	0
6"	0	1	3	3	6	8	13	14	13
8"	0	5	10	12	19	27	44	46	43
10"	1	13	26	29	48	67	107	112	105
12"	1	20	38	43	71	99	158	165	154
14"	2	27	52	58	96	133	213	223	208
16"	2	36	69	78	128	178	284	298	279
18"	3	43	83	93	153	214	341	358	334
20"	3	41	79	88	146	203	324	340	317
24"	12	166	319	357	587	818	1303	1367	1278

1.  $T_4$  values = in. lbs. per PSI $\Delta P$ .
2. All  $T_4$  values are positive acting to shut valve.
3. 0  $T_4$  values  $\cong < 1$ .

TABLE 9

CLASS 600 STD RATING



Seal Retaining Ring Upstream  
Disc Hydrodynamic Lift & Drag Torque -  $T_s$

VALVE SIZE	T <sub>s</sub> VS. DISC OPEN POSITION								
	10°	20°	30°	40°	50°	60°	70°	80°	90°
3"	0	0	0	0	0	0	0	0	0
4"	0	0	0	0	0	0	0	0	0
6"	0	0	1	2	3	2	0	-6	-13
8"	0	2	3	8	9	9	-2	-22	-43
10"	1	5	9	21	24	22	-6	-55	-105
12"	1	7	13	30	35	32	-9	-82	-154
14"	2	10	18	41	48	43	-12	-110	-208
16"	2	13	25	55	64	58	-16	-147	-279
18"	3	16	30	66	76	70	-20	-177	-334
20"	3	15	28	63	73	66	-19	-168	-317
24"	12	63	115	255	293	268	-76	-677	-1278

1.  $T_s$  values = in. lbs. per PSI  $\Delta P$ .
2. Except as noted,  $T_s$  values are positive acting to shut valve.
3. Negative (-)  $T_s$  values act to move the disc to the full open (90°) position.
4. 0  $T_s$  values  $\cong < 1$ .

### III. AERODYNAMIC TORQUE

Aerodynamic torque resulting from gaseous flow is negligible compared to Hydrodynamic torque. However, when in doubt concerning a specific application (such as applications where flow is sonic) consult the factory.

### IV. ACTUATOR SELECTION

Published torque values for Posi-Seal Trunnion Valves include adequate safety factors and do not require additional safety factors. However, when sizing actuators for specific valve torque requirements, decrease the published actuator torques by at least 10% to allow for a realistic safety factor in actuator selection. When selecting fail-safe actuators, the torque output at the end of the actuator spring stroke (ending torque) should be used as the basis for actuator selection. When the operating  $\Delta P$  used for actuator selection is less than maximum line pressure, contact the factory for sizing torque.