



SERV

Willbros Government Services, LLC
2087 E. 71st ST
TULSA, OKLAHOMA 74136

Welder or Welding Operator Performance Qualification (WPQ)

Welder's Name: Kotry, Justin Stamp: D
Test WPS No.: 1-S-6L Rev.: 0 WPQ No.: JK-S Date: 1/26/2012
Welding process(es) / type(s) used: SMAW / Manual
Type of joint welded: Plate Groove weld Joint type(s) qualified: Groove and Fillet Welds
Base metal(s) welded: SA-36 to SA-36

Table with 3 columns: Welder Variables (QW-350), Actual Values Used, Range Qualified. Rows include P- or S-Number, Base metal thickness, Pipe diameter, Backing, AWS classification, Filler metal specification, etc.

Table with 3 columns: Machine Welding Variables (QW-360), Actual Values Used, Range Qualified. Rows include Direct / remote visual control, Automatic voltage control, etc.

Fillet Welds: Qualified to make fillet welds of any size on all base material thicknesses and pipe diameters of any size.
\*\* Welds with backing include fillets and double-welded groove welds.
Notes: ( n1 ) Pipe with O.D. <= 24" limited to flat rotated & horizontal.

Guided Bend Test (QW-160)

Table with 4 columns: Figure Number and Type, Result, Figure Number and Type, Result. Rows show QW-462.2 Side bend tests with Satisfactory results.

Visual examination results: Visual exam satisfactory per QW-302.4 and QW-194
Volumetric test results: None
Welding test conducted by: Willbros Government Services, LLC
Mechanical/Radiographic tests conducted by: INSERV Lab test no.: W20120201

We certify that the statements in this record are correct and that the test welds were prepared, welded, and tested in accordance with the requirements of Section IX of the ASME Code.

Certified By: [Signature] Date: 2/1/2012 Quality Control
Organization: INTEGRATED SERVICE COMPANY, L.L.C.



Willbros Government Services, LLC  
 2087 E. 71st St  
 TULSA, OKLAHOMA 74136

**Welder or Welding Operator Performance Qualification (WPQ)**

Welder's Name: Kotry, Justin Stamp: D  
 Test WPS No.: 1-S-1 Rev.: 0 WPQ No.: JK-S1 Date: 2/21/2012  
 Welding process(es) / type(s) used: SMAW / Manual  
 Type of joint welded: Plate Groove weld Joint type(s) qualified: Groove and Fillet Welds  
 Base metal(s) welded: SA-516, Grade 70 to SA-516, Grade 70

Welder Variables (QW-350)	Actual Values Used	Range Qualified
P- or S-Number to P- or S-Number	P-No. 1 to P-No. 1	P-1 thru P-11, P-34 & P-4X
Base metal thickness (in.)	0.5	WPS Limits
Pipe diameter (in.)	N/A	2.875" minimum ( n1 )
	<b>SMAW / Manual</b>	<b>SMAW / Manual</b>
Backing **	No backing used	With or without backing
AWS classification	E7018	
Filler metal specification (SFA)	5.1	5.xx
Filler metal F-No.	4	F 4 (F 1 - F 3 w/backing)
Filler metal product form	N/A	N/A
Consumable insert	N/A	N/A
Deposit thickness (in.) [ $\geq 3$ layers]	0.5 [No]	1.0000" maximum
Welding position	2G, 3G, & 4G	All Positions
Weld progression	Vertical up	Vertical up (n4)
Backing gas	N/A	N/A

Machine Welding Variables (QW-360)	Actual Values Used	Range Qualified
Direct / remote visual control	N/A	N/A
Automatic voltage control	N/A	N/A
Automatic joint tracking	N/A	N/A
Welding position	N/A	N/A
Consumable insert	N/A	N/A
Backing **	N/A	N/A
Single / multiple pass per side	N/A	N/A

**Fillet Welds:** Qualified to make fillet welds of any size on all base material thicknesses and pipe diameters of any size.  
 \*\* Welds with backing include fillets and double-welded groove welds.  
**Notes:** ( n1 ) Pipe with O.D.  $\leq 24$ " limited to flat rotated & horizontal.  
 ( n4 ) The root pass, when removed to sound weld metal in preparation for welding the second side, and the cover or wash pass may be up or down.

**Guided Bend Test (QW-160)**

Figure Number and Type	Result	Figure Number and Type	Result
None		None	
None		None	
None		None	

Visual examination results: Visual exam satisfactory per QW-302.4 and QW-194  
 Radiographic test results: Acceptable Per QW-302.2 and QW-191  
 Welding test conducted by: Willbros Government Services, LLC  
 Mechanical/Radiographic tests conducted by: Pacific Island Inspection Lab test no.: JSO3272012C

We certify that the statements in this record are correct and that the test welds were prepared, welded, and tested in accordance with the requirements of Section IX of the ASME Code.

Certified By:  Organization: Willbros Government Services, LLC  
 T. Anderson Date: 3/27/2012 Quality Control



VISUAL INSPECTION & TESTING  
(VT) LEVEL II CERTIFICATION

THIS IS TO CERTIFY THAT:


*Justin Kotry*

HAS SUCCESSFULLY COMPLETED

*Visual Inspection & Testing  
(VT) Level II Technician / Competent Person*

THE CANDIDATE HAS SUCCESSFULLY COMPLETED ALL OF THE  
REQUIREMENTS FOR API 650/653 & ASNT SNT-TC-1A TRAINING.



  
Corporate ASNT Lvl III  
Willbros Government Services, LLC

2/29/2012

Date

PENETRANT TESTING (PT)  
LEVEL II CERTIFICATION

THIS IS TO CERTIFY THAT:


*Justin Kotry*

HAS SUCCESSFULLY COMPLETED

*Liquid Color Contrast Dye Penetrant Testing  
(PT) Level II Technician / Competent Person*

THE CANDIDATE HAS SUCCESSFULLY COMPLETED ALL OF THE  
REQUIREMENTS FOR API 650/653 & ASNT SNT-TC-1A TRAINING.



  
Corporate ASNT Lvl III  
Willbros Government Services, LLC

2/29/2012

Date



SERV

Willbros Government Services, LLC  
2087 E. 71st St  
TULSA, OKLAHOMA 74136

Welder or Welding Operator Performance Qualification (WPQ)

Welder's Name: Clark, Donald Stamp: C  
Test WPS No.: 1-M-IL Rev.: 0 WPQ No.: DC-M Date: 12/14/2011  
Welding process(es) / type(s) used: GMAW / Semiautomatic  
Type of joint welded: Plate Groove weld Joint type(s) qualified: Groove and Fillet Welds  
Base metal(s) welded: SA-36 to SA-36

Welder Variables (QW-350)	Actual Values Used	Range Qualified
P- or S-Number to P- or S-Number	P-No. 1 to P-No. 1	P-1 thru P-15F, P-34 & P-4X
Base metal thickness (in.)	0.5	WPS Limits
Pipe diameter (in.)	N/A	2.875" minimum ( n1 )
	<b>GMAW / Semiauto</b>	<b>GMAW / Semiauto</b>
Backing **	No backing used	With or without backing
AWS classification	ER70S-3	
Filler metal specification (SFA)	5.18	5.xx
Filler metal F-No.	6	F-No. 6
Filler metal product form	N/A	N/A
Consumable insert	N/A	N/A
Deposit thickness (in.) [ $\geq 3$ layers]	0.5 [No]	1.0000" maximum
Welding position	2G, 3G, & 4G	All Positions
Weld progression	Vertical up	Vertical up (n4)
Backing gas	No backing gas used	With or Without backing gas
GMAW / FCAW transfer mode	Spray arc	Spray, Pulsed, or Globular

Machine Welding Variables (QW-360)	Actual Values Used	Range Qualified
Direct / remote visual control	N/A	N/A
Automatic voltage control	N/A	N/A
Automatic joint tracking	N/A	N/A
Welding position	N/A	N/A
Consumable insert	N/A	N/A
Backing **	N/A	N/A
Single / multiple pass per side	N/A	N/A

Fillet Welds: Qualified to make fillet welds of any size on all base material thicknesses and pipe diameters of any size.  
\*\* Welds with backing include fillets and double-welded groove welds.  
Notes: ( n1 ) Pipe with O.D.  $\leq 24"$  limited to flat rotated & horizontal.  
( n4 ) The root pass, when removed to sound weld metal in preparation for welding the second side, and the cover or wash pass may be up or down.

Guided Bend Test (QW-160)

Figure Number and Type	Result	Figure Number and Type	Result
QW-462.2 Side bend	Satisfactory	QW-462.2 Side bend	Satisfactory
QW-462.2 Side bend	Satisfactory	QW-462.2 Side bend	Satisfactory
QW-462.2 Side bend	Satisfactory	QW-462.2 Side bend	Satisfactory

Visual examination results: Visual exam satisfactory per QW-302.4 and QW-194  
Volumetric test results: None  
Welding test conducted by: Willbros Government Services, LLC  
Mechanical/Radiographic tests conducted by: INSERV Lab test no.: W20120104

We certify that the statements in this record are correct and that the test welds were prepared, welded, and tested in accordance with the requirements of Section IX of the ASME Code.

Organization: INTEGRATED SERVICE COMPANY, L.L.C.

Certified By: David S. Glaves 1/4/2012 Quality Control  
Date



Willbros Government Services, LLC  
 2087 E. 71st St  
 TULSA, OKLAHOMA 74136

**Welder or Welding Operator Performance Qualification (WPQ)**

Welder's Name: Clark, Donald Stamp: C  
 Test WPS No.: 1-S-1 Rev.: 0 WPQ No.: DC-S1 Date: 2/21/2012  
 Welding process(es) / type(s) used: SMAW / Manual  
 Type of joint welded: Plate Groove weld Joint type(s) qualified: Groove and Fillet Welds  
 Base metal(s) welded: SA-516, Grade 70 to SA-516, Grade 70

Welder Variables (QW-350)	Actual Values Used	Range Qualified
P- or S-Number to P- or S-Number	P-No. 1 to P-No. 1	P-1 thru P-11, P-34 & P-4X
Base metal thickness (in.)	0.5	WPS Limits
Pipe diameter (in.)	N/A	2.875" minimum ( n1 )
	<b>SMAW / Manual</b>	<b>SMAW / Manual</b>
Backing **	No backing used	With or without backing
AWS classification	E7018	
Filler metal specification (SFA)	5.1	5.xx
Filler metal F-No.	4	F 4 (F 1 - F 3 w/backing)
Filler metal product form	N/A	N/A
Consumable insert	N/A	N/A
Deposit thickness (in.) [ $\geq 3$ layers]	0.5 [No]	1.0000" maximum
Welding position	2G & 4G	Flat, Horizontal, & Overhead
Weld progression	N/A	N/A
Backing gas	N/A	N/A

Machine Welding Variables (QW-360)	Actual Values Used	Range Qualified
Direct / remote visual control	N/A	N/A
Automatic voltage control	N/A	N/A
Automatic joint tracking	N/A	N/A
Welding position	N/A	N/A
Consumable insert	N/A	N/A
Backing **	N/A	N/A
Single / multiple pass per side	N/A	N/A

**Fillet Welds:** Qualified to make fillet welds of any size on all base material thicknesses and pipe diameters of any size.  
 \*\* Welds with backing include fillets and double-welded groove welds.  
**Notes:** ( n1 ) Pipe with O.D.  $\leq 24$ " limited to flat rotated & horizontal.

**Guided Bend Test (QW-160)**

Figure Number and Type	Result	Figure Number and Type	Result
None		None	
None		None	
None		None	

Visual examination results: Visual exam satisfactory per QW-302.4 and QW-194  
 Radiographic test results: Acceptable Per QW-302.2 and QW-191  
 Welding test conducted by: Willbros Government Services, LLC  
 Mechanical/Radiographic tests conducted by: Pacific Island Inspection Lab test no.: JSO3272012B

We certify that the statements in this record are correct and that the test welds were prepared, welded, and tested in accordance with the requirements of Section IX of the ASME Code.

Certified By:  Organization: Willbros Government Services, LLC  
 T. Anderson Date: 3/27/2012 Quality Control

VISUAL INSPECTION & TESTING  
(VT) LEVEL II CERTIFICATION

THIS IS TO CERTIFY THAT:

*Donald Clark*

HAS SUCCESSFULLY COMPLETED

*Visual Inspection & Testing  
(VT) Level II Technician / Competent Person*

THE CANDIDATE HAS SUCCESSFULLY COMPLETED ALL OF THE  
REQUIREMENTS FOR API 650/653 & ASNT SNT-TC-1A TRAINING.



Corporate ASNT Lvl III  
Willbros Government Services, LLC

9/30/2011

Date

PENETRANT TESTING (PT)  
LEVEL II CERTIFICATION

THIS IS TO CERTIFY THAT:


*Donald Clark*

HAS SUCCESSFULLY COMPLETED

*Liquid Color Contrast Dye Penetrant Testing  
(PT) Level II Technician / Competent Person*

THE CANDIDATE HAS SUCCESSFULLY COMPLETED ALL OF THE  
REQUIREMENTS FOR API 650/653 & ASNT SNT-TC-1A TRAINING.



  
Corporate ASNT Lvl III  
Willbros Government Services, LLC

9/30/2011

Date





SERV

Willbros Government Services, LLC

2087 E. 71st St

TULSA, OKLAHOMA 74136

Welder or Welding Operator Performance Qualification (WPQ)

Welder's Name: Chapman, Robert Stamp: B

Test WPS No.: 1-M-1L Rev.: 0 WPQ No.: RC-M

Date: 12/14/2011

Welding process(es) / type(s) used: GMAW / Semiautomatic

Type of joint welded: Plate Groove weld Joint type(s) qualified: Groove and Fillet Welds

Base metal(s) welded: SA-36 to SA-36

Welder Variables (QW-350)	Actual Values Used	Range Qualified
P- or S-Number to P- or S-Number	P-No. 1 to P-No. 1	P-1 thru P-15F, P-34 & P-4X
Base metal thickness (in.)	0.5	WPS Limits
Pipe diameter (in.)	N/A	2.875" minimum (n1)
	GMAW / Semiauto	GMAW / Semiauto
Backing **	No backing used	With or without backing
AWS classification	ER70S-3	
Filler metal specification (SFA)	5.18	5.xx
Filler metal F-No.	6	F-No. 6
Filler metal product form	N/A	N/A
Consumable insert	N/A	N/A
Deposit thickness (in.) [ $\geq 3$ layers]	0.5 [No]	1.0000" maximum
Welding position	2G, 3G, & 4G	All Positions
Weld progression	Vertical up	Vertical up (n4)
Backing gas	No backing gas used	With or Without backing gas
GMAW / FCAW transfer mode	Spray arc	Spray, Pulsed, or Globular

Machine Welding Variables (QW-360)	Actual Values Used	Range Qualified
Direct / remote visual control	N/A	N/A
Automatic voltage control	N/A	N/A
Automatic joint tracking	N/A	N/A
Welding position	N/A	N/A
Consumable insert	N/A	N/A
Backing **	N/A	N/A
Single / multiple pass per side	N/A	N/A

Fillet Welds: Qualified to make fillet welds of any size on all base material thicknesses and pipe diameters of any size.  
 \*\* Welds with backing include fillets and double-welded groove welds.  
 Notes: ( n1 ) Pipe with O.D.  $\leq 24$ " limited to flat rotated & horizontal.  
 ( n4 ) The root pass, when removed to sound weld metal in preparation for welding the second side, and the cover or wash pass may be up or down.

Guided Bend Test (QW-160)

Figure Number and Type	Result	Figure Number and Type	Result
QW-462.2 Side bend	Satisfactory	QW-462.2 Side bend	Satisfactory
QW-462.2 Side bend	Satisfactory	QW-462.2 Side bend	Satisfactory
QW-462.2 Side bend	Satisfactory	QW-462.2 Side bend	Satisfactory

Visual examination results: Visual exam satisfactory per QW-302.4 and QW-194

Volumetric test results: None

Welding test conducted by: Willbros Government Services, LLC

Mechanical/Radiographic tests conducted by: INSERV

Lab test no.: W20120104

We certify that the statements in this record are correct and that the test welds were prepared, welded, and tested in accordance with the requirements of Section IX of the ASME Code.

Organization: INTEGRATED SERVICE COMPANY, L.L.C.

Certified By:

*D. Galves*  
David S. Galves

1/4/2012

QC Manager

Date



Willbros Government Services, LLC  
 2087 E. 71st St  
 TULSA, OKLAHOMA 74136

**Welder or Welding Operator Performance Qualification (WPQ)**

Welder's Name: Chapman, Robert Stamp: B  
 Test WPS No.: 1-S-1 Rev.: 0 WPQ No.: RC-S1 Date: 2/21/2012  
 Welding process(es) / type(s) used: SMAW / Manual  
 Type of joint welded: Plate Groove weld Joint type(s) qualified: Groove and Fillet Welds  
 Base metal(s) welded: SA-516, Grade 70 to SA-516, Grade 70

Welder Variables (QW-350)	Actual Values Used	Range Qualified
P- or S-Number to P- or S-Number	P-No. 1 to P-No. 1	P-1 thru P-15F, P-34 & P-4X
Base metal thickness (in.)	0.5	WPS Limits
Pipe diameter (in.)	N/A	2.875" minimum ( n1 )
	<b>SMAW / Manual</b>	<b>SMAW / Manual</b>
Backing **	No backing used	With or without backing
AWS classification	E7018	
Filler metal specification (SFA)	5.1	5.xx
Filler metal F-No.	4	F 4 (F 1 - F 3 w/backing)
Filler metal product form	N/A	N/A
Consumable insert	N/A	N/A
Deposit thickness (in.) [ $\geq 3$ layers]	0.5 [No]	1.0000" maximum
Welding position	2G, 3G, & 4G	All Positions
Weld progression	Vertical up	Vertical up (n4)
Backing gas	N/A	N/A

Machine Welding Variables (QW-360)	Actual Values Used	Range Qualified
Direct / remote visual control	N/A	N/A
Automatic voltage control	N/A	N/A
Automatic joint tracking	N/A	N/A
Welding position	N/A	N/A
Consumable insert	N/A	N/A
Backing **	N/A	N/A
Single / multiple pass per side	N/A	N/A

**Fillet Welds:** Qualified to make fillet welds of any size on all base material thicknesses and pipe diameters of any size.  
 \*\* Welds with backing include fillets and double-welded groove welds.  
**Notes:** ( n1 ) Pipe with O.D.  $\leq 24$ " limited to flat rotated & horizontal.  
 ( n4 ) The root pass, when removed to sound weld metal in preparation for welding the second side, and the cover or wash pass may be up or down.

**Guided Bend Test (QW-160)**

Figure Number and Type	Result	Figure Number and Type	Result
None		None	
None		None	
None		None	

Visual examination results: Visual exam satisfactory per QW-302.4 and QW-194  
 Volumetric test results: Acceptable Per QW-302.2 and QW-191  
 Welding test conducted by: Willbros Government Services, LLC  
 Mechanical/Radiographic tests conducted by: Pacific island Inspection - RT Lab test no.: JSO3272012A

We certify that the statements in this record are correct and that the test welds were prepared, welded, and tested in accordance with the requirements of Section IX of the ASME Code.

Certified By:  Organization: Willbros Government Services, LLC  
 T. Anderson Date: 3/27/2012 Quality Control

PENETRANT TESTING (PT)  
LEVEL II CERTIFICATION

THIS IS TO CERTIFY THAT:


*Robert Chapman*

HAS SUCCESSFULLY COMPLETED

*Liquid Color Contrast Dye Penetrant Testing  
(PT) Level II Technician / Competent Person*

THE CANDIDATE HAS SUCCESSFULLY COMPLETED ALL OF THE  
REQUIREMENTS FOR API 650/653 & ASNT SNT-TC-1A TRAINING.



  
Corporate ASNT Lvl III  
Willbros Government Services, LLC

11/30/2010

Date

VISUAL INSPECTION & TESTING  
(VT) LEVEL II CERTIFICATION

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THIS IS TO CERTIFY THAT:

*Robert Chapman*

HAS SUCCESSFULLY COMPLETED

*Visual Inspection & Testing  
(VT) Level II Technician / Competent Person*

---

THE CANDIDATE HAS SUCCESSFULLY COMPLETED ALL OF THE  
REQUIREMENTS FOR API 650 / 653 & ASNT SNT-TC-1A TRAINING.



Corporate ASNT Lvl III  
Willbros Government Services, LLC

10/29/2010

Date



**Willbros Government Services, LLC.**  
**DAILY PRODUCTION REPORT**  
 (ATTACH ADDITIONAL SHEETS IF NECESSARY)

**DATE:** 16 January 2013

<b>CONTRACT #:</b>	N 62583-09-D-0132/0003	<b>TITLE AND LOCATION:</b>	Red Hill Complex – Pearl Harbor NAVSTA	<b>REPORT NO.:</b>	54118
<b>WGS PROJECT #:</b>	54118	<b>Tank 5 &amp; 17</b>	Pearl Harbor, HI		
<b>SITE MANAGER:</b>	James Hagen	<b>REPRESENTATIVE:</b>	Marc Steinhebel ( NFEXWC – NTR)		
<b>AM WEATHER:</b>	Cloudy	<b>PM WEATHER:</b>	Sunny	<b>MAX. TEMP:</b>	79
				<b>MIN. TEMP:</b>	70

**WORK PERFORMED TODAY**

Willbros Government Services, LLC (WGS) continued performing work activities / task per the NAVFAC Contract N62583-09-D-0132/ Task Order 0003 and approved contract modifications.

**TASK**

**TK5** – Fabrication of the new 4” drain line and 3/4 sample line on the exterior of TK 5 is on hold until coating activities are completed.  
 A&S began abrasive blasting in TK 5  
 NACE inspector Frank Bringas performed final inspection on areas where grinding was done for coating process.  
 API inspection was performed by Tim Anderson on areas where grinding was done for coating process.  
 WGS continued prepping for TK 5 commissioning once coating activities are complete.

**TK 17** – No work in TK 17 today.

<b>SAFETY</b>	WAS A JOB SAFETY MEETING HELD THIS DATE?	<input checked="" type="checkbox"/>	YES	<input type="checkbox"/>	NO	TOTAL WORK HOURS ON THE JOB SITE FOR THIS DATE:	131
	WERE THERE ANY LOST TIME ACCIDENTS THIS DATE?	<input type="checkbox"/>	YES	<input checked="" type="checkbox"/>	NO		
	WAS CRANE/TRENCHING/SCAFFOLD/HV ELECTRICAL/HIGH WORK DONE?	<input checked="" type="checkbox"/>	YES	<input type="checkbox"/>	NO	CUMULATIVE TOTAL OF WORK HOURS FROM PREVIOUS REPORTS:	49,965
	WAS HAZARDOUS MATERIAL/WASTE RELEASED INTO THE ENVIRONMENT?	<input type="checkbox"/>	YES	<input checked="" type="checkbox"/>	NO	TOTAL WORK HOURS FROM START OF CONSTRUCTION:	50,096

**SAFETY**

LIST SAFETY ACTIONS TAKEN TODAY / SAFETY INSPECTIONS CONDUCTED  Yes  SAFETY REQUIREMENTS HAVE BEEN MET.

WGS observed and monitored the proper PPE was utilized and all expected safety procedures followed.  
 Federal Fire Dept. has issued hot work permits for designated areas. WGS performed gas testing and continuous monitoring in relevant work areas.

**CONCERNS**

REMARKS / UNRESOLVED ISSUES / ANY SCHEDULE IMPACTS / PROJECT DELAYS



**WGS LABOR SITE SUMMARY**

CRAFT / TRADE NAME	EMPLOYER		TIME		TOTAL HOURS
			On Site	Off Site	
Site Manager / Supt.	WGS	James Hagen / John Sebok	12	0	12
Health & Safety Officer (HSO)	WGS	John Sebok / James Hagen	6	0	6
Quality Control Manager (QCM)	WGS	James Hagen	6	0	6
Quality Control Inspector	WGS		0	0	0
Laborer – Cleaning / Civil / Mechanical	WGS		94	0	94
Boilermaker – Fitter / Welder	WGS		0	0	0
Piping - Fitter / Welder	WGS		0	0	0
Clerical	WGS		8	0	8
API / QC Inspector	WGS		5	0	5
NDE Inspector / Tech	WGS		0	0	0

**EQUIPMENT / MATERIAL RECEIVED TODAY TO BE INCORPORATED INTO WORK**

DESCRIPTION	QUANTITY	SHIPPING DOCUMENTS
Consumable / Tools / Supplies		

**WGS CONSTRUCTION AND PLANT EQUIPMENT ON THE JOB SITE TODAY**

DESCRIPTION	IDLE	RENTED / OWNED	QUANTITY	On Site HRS	Off Site HRS	TOTAL HOURS
Trucks / Vehicles / Golf Cart		O-4/R-2	6	10		10
Office Trailer & Conexes (2) & Hand Tools & Equipment		O	Lot	10		10
Booms & Jacking Stands		O	Lot	10		10
Air Compressors		R	2	10		10
Forklift		R	1	10		10
Welding machines		O	2	10		10

**SUBCONTRACTORS ONSITE TODAY**

COMPANY	# OF PERSONNEL	WORK PERFORMED
Abhe & Svoboda	5	Dust collection fabrication
CSI	1	NACE Inspector

**GENERAL COMMENTS / REMARKS**

Site Visitor's – XXXXXXXXXX

A&S began abrasive blasting in TK 5  
 NACE inspector Frank Bringas performed final inspection on areas where grinding was done for coating process to ensure all weld spatter had been removed. Two areas of concern were noted and Abhe & Svoboda addressed these areas prior to starting the abrasive blasting.  
 API inspection was performed by Tim Anderson on areas where grinding was done for coating process to ensure wall thickness was acceptable. No concerns were noted.

James Hagen  
 Printed Name – Site Manager

Joe Gilbert  
 Printed Name – Project Manager

16 January 2013  
 Date



<b>CONTRACT ORDER NO.:</b> N 62583-09-D-0132/0003	<b>CONTRACTOR QUALITY CONTROL REPORT</b> (ATTACH ADDITIONAL SHEETS)	<b>REPORT NO.:</b> 54118	<b>DATE:</b> 16 January 2013
<b>Tank 5 &amp; 17</b>			

PHASE	Y=YES, N=NO, SEE REMARKS; BLANK-NOT APPLICABLE		IDENTIFY DEFINABLE FEATURE OF WORK LOCATION AND LIST PERSONNEL PRESENT
<b>P R E P A R A T O R Y</b>	THE PLANS AND SPECS HAVE BEEN REVIEWED	Y	<u>Work Location:</u> ADIT 4 & 5 / Tank 5 & 17
	THE SUBMITTALS HAVE BEEN APPROVED.	Y	<u>Pre-Work Evaluation/Site Preparation:</u> TK 5 – LOTO of piping connections and tie-ins
	MATERIALS COMPLY WITH APPROVED SUBMITTALS.	Y	TK 17 – -LOTO of piping connections and tie-ins -Ventilation of tank
	MATERIALS ARE STORED PROPERLY.	Y	
	PRELIMINARY WORK WAS DONE CORRECTLY.	Y	
	TESTING PLAN HAS BEEN REVIEWED.	Y	
	WORK METHOD AND SCHEDULE DISCUSSED	Y	

PHASE	Y=YES, N=NO, SEE REMARKS; BLANK-NOT APPLICABLE		<u>Work Location &amp; Task:</u>	TESTING PERFORMED & WHO PERFORMED TEST
<b>I N I T I A L</b>	PRELIMINARY WORK WAS DONE CORRECTLY	Y	Tank 5 – Abrasive Blasting Grinding weld spatter	NACE pre blast ins. Frank Bringas CSI API final ins. before coating. Tim Anderson WGS
	SAMPLE HAS BEEN PREPARED / APPROVED.	X		
	WORKMANSHIP IS SATISFACTORY.	Y	Tank 17 – Tell-tale repairs	None
	TEST RESULTS ARE ACCEPTABLE.	Y		
	WORK IS IN COMPLIANCE WITH THE CONTRACT.	Y		

PHASE	Y=YES, N=NO, SEE REMARKS; BLANK-NOT APPLICABLE			TESTING PERFORMED & WHO PERFORMED TEST
<b>F O L L O W U P</b>	WORK COMPLIES WITH CONTRACT AS APPROVED IN INITIAL PHASE.			None
	NO REPAIRS OR REWORK NECESSARY			

REWORK ITEMS IDENTIFIED TODAY  
(NOT CORRECTED BY CLOSE OF BUSINESS)

REWORK ITEMS CORRECTED TODAY  
(FROM REWORK ITEMS LIST)

Remarks:

ON BEHALF OF THE CONTRACTOR, I CERTIFY THIS REPORT IS COMPLETE AND CORRECT AND EQUIPMENT AND MATERIAL USED AND WORK PERFORM DURING THIS REPORTING PERIOD IS IN COMPLIANCE WITH THE CONTRACT DRAWINGS AND SPECIFICATIONS TO THE BEST OF KNOWLEDGE EXCEPT IN THIS REPORT.

James Hagen  
PRINT NAME OF SITE MANAGER

James Hagen  
PRINTED NAME OF AUTHORIZED QC MANAGER

16 January 2013  
DATE

**GOVERNMENT QUALITY ASSURANCE REPORT**

DATE

QUALITY ASSURANCE REPRESENTATIVE'S REMARKS AND/OR EXCEPTIONS TO THE REPORT

PRINT NAME OF GOVERNMENT QA REPRESENTATIVE

GOVERNMENT QA REPRESENTATIVE

DATE

PROJECT TITLE  
Clean, Inspect and Repair Fuel Tanks  
Redhill Complex, Pearl Harbor HI

SITE PHOTOGRAPHS

TK 5 dust collection unit blower motor



Lower tunnel conditions during blasting



TK 5 dust collection unit filter housing



Lower tunnel conditions during blasting





**DEPARTMENT OF THE NAVY**  
NAVAL FACILITIES ENGINEERING AND EXPEDITIONARY WARFARE CENTER  
1000 23RD AVENUE  
PORT HUENEME CA 93043-4301

N REPLY REFER TO:  
4200/AQ71  
SER 0228  
4 FEBB 2014

WILLBROS GOVERNMENT SERVICES (U.S.), LLC  
Attn: Rick Grossman  
2087 E 71ST STE 101  
Tulsa, OK, 74136-5462

Dear Mr. Grossman:

Subject: CONTRACT N62583-09-D-0132 TASK ORDER 0003, CLEAN, INSPECT, REPAIR  
TANKS 5 AND 17, REDHILL, PEARL HARBOR HAWAII

There is an apparent loss of product in Tank 5 which was repaired under the subject contract task order. After preliminary investigation the Government has determined that the loss of product most likely resulted from a leak caused by defects in material or workmanship in the performance of the task order. I am therefore evoking my remedies under the Warranty of Construction Clause (FAR 52.246-21) and directing Willbros to identify and correct the deficiency(ies) in Tank 5.

Within ten calendar days of receipt of this letter, Willbros shall provide an written work plan that identifies the means, methods and proposed schedule for re-entering Tank 5. Willbros shall also identify any requirements necessary for Willbros to provide Tank 5 access to government personnel, and/or representatives of the Government. Willbros shall not proceed to mobilize or enter the tank until the Work Plan is accepted by the Government and a Notice to Proceed is issued by the contracting officer.

The preliminary investigation has provided the following information:

- The operators of the tank reported a loss of product during initial filling operations, and the gauging logs show a loss of product over the 30-day period.
- There was a re-appearance of fuel on the lower tunnel wall after the tank was refueled.
- The monitoring well nearest to Tank 5 has shown a significant spike in petroleum products.
- The Government has determined that proper procedures were followed when refilling the tank.
- The Government has determined that the SPAWAR contractor that installed the Automated Fuel Handling Equipment was not performing work that could have damaged the tank.

4200/AQ71  
SER 0228  
4 Feb 2014

If, during the course of any inspections or other work on the tank, Willbros determines that the leak was caused by reasons other than defective materials or workmanship provided by Willbros, you are directed to stop all further inspections and immediately notify the contracting officer.

If you have any questions please contact me at (b) (6) or (805)382-3140.

Sincerely,

(b) (6)  
(b) (6)  
(b) (6)



**DEPARTMENT OF THE NAVY**  
NAVAL FACILITIES ENGINEERING AND EXPEDITIONARY WARFARE CENTER  
1000 23RD AVENUE  
PORT HUENEME CA 93043-4301

IN REPLY REFER TO:

4200/AQ72  
SER 0016  
16 Oct 2014

WILLBROS GOVERNMENT SERVICES (U.S.), LLC  
Attn: Rick Grossman  
2087 E 71ST STE 101  
Tulsa, OK, 74136-5462

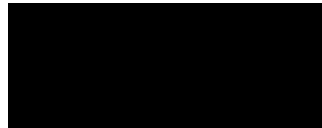
Subject: CONTRACT N62583-09-D-0132 TASK ORDER 0003, CLEAN, INSPECT, REPAIR TANKS 5 AND 17, REDHILL, PEARL HARBOR HAWAII; NOTICE TO PROCEED

This notice constitutes a Notice To Proceed (NTP) for the subject project, effective 20 Oct 2014. No work may proceed before that date. This NTP is for the warranty work, specifically the search for free product and inspection of repairs, as detailed in Revision 12 of the work plan.

You are reminded that the work plan has a hold-point (Activity ID #17) for Government review of your findings. No work on repairs may proceed until expressly authorized by the undersigned.

You are requested to submit a CPM schedule update that reflects the change of the start date.

If there are any questions pertaining to this matter, please contact me at [REDACTED] or via email at [REDACTED].







**WILLBROS GOVERNMENT SERVICES (U.S.), LLC**

A WILLBROS COMPANY

12 February 2015

To Whom It May Concern:

Willbros Government Services has completed the Modified API 653 Visual Inspection of TK 5 as described in Section 4.5 PROJECT TASK AND SEQUENCES of the TK 5 Warranty Work Plan. The inspection was performed by WGS QC Manager Matt Halderman, who currently holds API 653 Certification #42276 as well as AWS CWI Certification #08110741.

The results of this Visual Inspection are as follows:

A total of Six Hundred Seventy-Seven (677) previous repair locations were checked in TK 5 per the procedures outlined in the TK 5 Warranty Work Plan Scope of Work (SOW). Five Hundred Sixteen (516) of the previous repair locations failed to meet the acceptance criteria outlined in the SOW. The remaining One Hundred Sixty-One (161) previous repair locations passed per the acceptance/rejection criteria as described in the SOW. During this process the entire tank was inspected for any other rejectable conditions. Six (6) new locations were flagged for possible rejection and one (1) previous weld repair (WR165) was found in the tank, but was discovered to be missing from the QC Log. The six (6) new locations have been added to the QC Log for future repair and the one (1) old WR has also been inserted into the log in its proper location. The six (6) new locations added to the QC Log are as follows:

Repair Number	Row/Plate	Indication
1. WWP 013	A/28	Gouge needs Plate
2. WWP 014	A/28	Gouge needs Plate
3. WWP 015	B/01	Old Repair (not WGS) needs Plate
4. WWP 016	15/12	Old Repair (not WGS) needs Re-Welded
5. WWP 017	E2/P4	Dent needs Plate
6. WWR 018	C/47	Original Grout Nozzle needs Re-Welded

In summary, WGS rejected 76% of our previous repairs based on our Visual Inspection. The criteria used for rejecting these locations include causes such as Undercut, Underfill, Lack of Fusion, and Excessive Reinforcement or Grinding. As the inspection continues with MT and LT, any new information concerning the currently failed locations will be addressed in future reports.

Should you need more information please feel free to contact me at the number or email below.

Very Respectfully,

**James Hagen**  
Project Manager  
Cell: 808-738-6396  
E-mail: [james.hagen@willbros.com](mailto:james.hagen@willbros.com)

[james.hagen@willbros.com](mailto:james.hagen@willbros.com)  
Digitally signed by  
james.hagen@willbros.com  
DN: cn=james.hagen@willbros.com  
Date: 2015.02.17 08:53:26 -10'00'

**Matt Halderman**  
QC Manager  
Cell: 918-556-3603  
E-mail: [matt.halderman@willbros.com](mailto:matt.halderman@willbros.com)





## WILLBROS GOVERNMENT SERVICES (U.S.), LLC

A WILLBROS COMPANY

20 August 2015

To Whom It May Concern:

Willbros Government Services has completed the Mag Particle (MT) and Vacuum Box (LT) Inspection of TK 5 as described in Section 4.5 PROJECT TASK AND SEQUENCES of the TK 5 Warranty Work Plan. The inspection was performed by WGS Level II NDE Technicians under the direction of QC Manager Matt Halderman.

The results of this MT and LT Inspection are as follows:

A total of Six Hundred Eighty Two (682) previous repair locations were checked in TK 5 per the procedures outlined in the TK 5 Warranty Work Plan Scope of Work (SOW). Reconciliations were made to the QC Log as discrepancies in numbering were found in comparison to the log dated 12 February 2015. All Six Hundred Eighty Two (682) of the previous repair locations failed to meet the acceptance criteria outlined in the SOW for the MT examination. Four Hundred Fifteen (415) of Four Hundred Seventy Nine (479) locations Passed Vacuum Box Leak Testing (LT), Two Hundred Three (203) locations were unable to be tested due to geometry of the repair. Sixty Four (64) locations failed the Vacuum Box Leak Test. During this process other welds in close proximity to the WGS repairs were also tested and inspected for any other rejectable conditions. Some locations showed linear indications in the adjacent existing welds; none of these failed the vacuum box test.

All failed locations will be repaired per the API 653 Code specifications as outlined in the WP and all indications in adjacent welds will be covered in this process. Some of the previous repair plates will be completely removed and replaced and some will be repaired by removing a portion of the existing weld and re-welding to an acceptable condition per the code.

In summary, WGS rejected 100% of our previous repairs based on our Mag Particle Inspection. The upcoming repairs will be made per API 653 Code specifications and weld spacing/plate shape will be addressed on a case by case basis as there are several different configurations that will require different methods to address criteria used for accepting or rejecting these locations.

Should you need more information please feel free to contact me at the number or email below.

Very Respectfully,

James Hagen  
Project Manager  
Cell: 808-738-6396  
E-mail: [james.hagen@willbros.com](mailto:james.hagen@willbros.com)

james.hagen@  
willbros.com

Digitally signed by  
james.hagen@willbros.com  
DN: cn=james.hagen@willbros.com  
Date: 2015.08.20 10:28:51 -10'00'

Matt Halderman  
QC Manager  
Cell: 918-556-3603  
E-mail: [matt.halderman@willbros.com](mailto:matt.halderman@willbros.com)



**APPENDIX M**

**PROJECT DATA –  
POTENTIAL FREE PRODUCT RECLAMATION PLAN**



Distribution is limited to US Government agencies and their contractors; administrative/operational use within the context of this project. Other request shall be referred to the Naval Facilities Engineering Service Center.



**RED HILL COMPLEX PROJECT**  
**TANK 5 WARRANTY WORK**  
**IDENTIFICATION / REMOVAL OF POTENTIAL FREE PRODUCT**

**1.0 IDENTIFICATION / REMOVAL OF POTENTIAL FREE PRODUCT SUMMARY**

Willbros Government Services has prepared this procedure under Contract No. N62583-09-D-0132 / TO 003 for warranty work on Tank 5 located at Red Hill Pearl Harbor, HI. This procedure will be utilized to identify potential free product and provide guidance for the removal, storage, and disposal of any potential reclaimed free product thought to have been lost during Tank 5 filling activities.

Note – For any additional information not listed in this document see the WGS WP, specifically the Repair Procedure.

**2.1 POTENTIAL FREE PRODUCT- IDENTIFICATION SUMMARY**

Due to the underground construction of Tank 5, some of the exterior surfaces are inaccessible for gas free testing and permitting. Areas of the tank's internal steel liner appear to have separated from the concrete encasement surrounding the tank. This condition can allow water, fuel, liquid or vapor, to be trapped in a localized area between the two surfaces. WGS intends to identify potential trapped free product in these areas via Vacuum Box Testing (VBT). This will be conducted to verify the integrity of the repair plate seal welds made to the tanks interior surface, as well as, identifying the existence of free product trapped in that location. All previous repairs performed by WGS will be VBT'd during this process including the 17 failed locations previously identified in the initial inspection. Any area suspected of holding trapped free product, that does not have a repair location suitable for VBT, will be addressed using an alternate method requiring WGS to drill a new inspection port to conduct the test.

The tank is divided into 4 quadrants (A, B, C, D) which identify the tank left to right. The tank is also divided from bottom to top by Lower Dome, Shell or Barrel, Extension Rings, and Upper Dome. WGS intends to drill and/or expose a minimum of 12 inspection ports in the tank liner; 1 port per quadrant for the Extension Rings, Shell or Barrel, and Lower Dome. Due to initial tank filling procedures and gravity WGS does not expect free product to be located in the Upper Dome. Coating will be removed and replaced as-needed on the lower dome.

**2.2 FREE PRODUCT IDENTIFICATION PROCEDURE**

Free Product Identification – Steps & Sequence

- 2.2.1 Vacuum Box Testing- During VBT the presence of product being pulled from behind the repair plate or the odor of product after the Vacuum Box is removed from the test area will be recorded in the QC log by the NDE technicians performing the test.
- 2.2.2 Inspection Port Determination- WGS QC Manager will review the NDE data collected to determine locations for the minimum 12 additional inspection ports, distributed in the tank as described in Section 2.1, based on the NDE data and tank conditions. If the QC manager is unable to satisfy the criteria using existing repairs, he will determine locations for new inspection ports, using the alternate method described in Section 2.1, based on the NDE data and tank conditions e.g., liner separation, leak path, presence of product or odor etc.
- 2.2.3 Tracking Inspection Ports- WGS will use the QC Log to track the location of each plate removed and/or port drilled for the purpose of identifying potential free product.



## 2.3 FREE PRODUCT RECLAMATION PROCEDURE

### Product Reclamation – Steps & Sequence

2.3.1 Repair Plate Location – If liquid is detected behind a repair plate, a port will be drilled in close proximity to drain any product found at the location.  
(See 2.2.3.2 for draining procedure)

2.3.2 Alternate Method: New Inspection Port Location – New locations will be determined by the QC Manager based on Section 2.1, Section 2.2.2 and the NDE data and conditions found in the tank. A port, 1/4" in diameter, will be created in the designated location with a pneumatic drill.

### 2.3.3 Product Reclamation-

2.2.3.1- **If no liquid is present-** WGS will test the area through the port with a gas monitor and record the readings on the QC log to be reviewed by the QC Manager to determine if further action is required.

2.2.3.2- **Liquid present-** Inspection port will be drilled and tapped to install a threaded valve to allow WGS to perform controlled draining of liquids. During tapping and threading of inspection port WGS will place oil absorbent rags below inspection port to catch any seeping liquid. A 15 gallon DOT drum will be located inside of the man basket and will be the temporary storage container until personnel return to the catwalk and material can be relocated into a larger drum or container. Once gravity flow through the valve has stopped, WGS will attempt to extract any additional accessible liquid with a small vacuum pump (5-10 Hg psig). Liquids will be collected in containers or drums to be evacuated from the tank thru the access tunnel.

2.2.3.3- WGS will track and record the amount collected and disposed of in the QC log. Testing will be performed on any collected liquids to characterize and determine proper disposal procedures, e.g., fuel reclamation or waste. Disposal location and test results will be noted in the QC log. Photos and visual characterizations will be documented in the QC daily reports.

*Note –This process will begin at the top of the tank and proceed downward to limit or control the amount of liquids drained from any location where they are encountered. Based on the construction methods and historical data relating to the tank WGS does not expect to find large quantities of product in any single location of the tank. During the process described above, if WGS encounters a quantity of product that is not feasible to drain in the described method, the test/drain port will be plugged and another procedure will be developed based on the location and condition of the area where the product is found.*

## 2.4 Product Inspection Port Repairs

Product inspection port repairs will conform to WGS Work Plan Tank 5 Repair Procedure rev 1D and the following. An area will be marked or laid out a minimum of 1" beyond the inspection port peripheral edge. The entire surface of the marked area will be cleaned to remove all existing coating or debris from the weld area. A groove will be ground into the port in accordance with the WPS joint limits, and then filled with weld, back to base metal thickness. After cleaning the filled groove, a weld overlay will be performed on the repair location. All weld overlays should extend a minimum of 1" horizontally and 1/2" vertically on either side of the affected area designated for overlay.

## 2.5 Summary

Willbros will perform the above procedures to identify, reclaim, or dispose of any potential free product thought to have been lost during Tank 5 filling activities. Areas identified as inspection ports during the performance of this procedure will be tracked in the QC log, which will be submitted to EXWC with the Inspection Report prior to beginning any tank repairs.



## **WILLBROS GOVERNMENT SERVICES (U.S.), LLC**

A WILLBROS COMPANY

06 November 2014

To Whom It May Concern:

Willbros Government Services has completed the Free Product Reclamation Procedure described in Appendix M of the TK 5 Warranty Work Plan. No free product was located or collected during this recovery operation. A total of thirteen (13) locations were checked in TK 5 per the procedures outlined in Appendix M. Twelve (12) were new locations created in each quadrant and elevation of the tank and one (1) was an existing location uncovered, by the previous removal of a repair plate, during the initial leak investigation inspection. The results of this operation have been recorded in the QC Log and the details are described in the following pages with field notes, sketches and photographs. If free product is encountered in the future, as we continue our inspection and repairs in TK 5, the procedures outlined in Appendix M will be utilized to recover and collect said product and should it occur, this activity will be documented and recorded in the same fashion as described above.

Should you need more information please feel free to contact me at the number or email below.

Very Respectfully,

**James Hagen**  
**Project Manager**  
**Willbros Government Services, LLC**

Cell: [REDACTED]

Fax: 918-481-4317

E-mail: [james.hagen@willbros.com](mailto:james.hagen@willbros.com)



**Willbros Government Services, (U.S.) LLC**

A Willbros Company

Date: 10/30/14

Subject: Potential Free Product Recovery Notes

Summary:

WGS used various criteria to identify and locate Potential Free Product Recovery ports including previous LT testing results, sounding for hollow spots indicating voids between the steel liner and concrete encasement, and the location of previous repairs.

Steps taken were as follows:

- 1) Determine Port Location
- 2) Drill Port
- 3) Test port for presence of hydrocarbons
- 4) Vacuum drilled port
- 5) Re-test port for presence of hydrocarbons

\*Please see notes below for each port.

**001- C1-P2 Lower Dome Quadrant A:**

This area was chosen because of its relation to 32" issue / receipt lines exiting the tank to lower level. Sounding located a hollow spot.

- 1) Course C1 Plate 2
- 2) Dry / no liquid (1/8" clearance behind plate)
- 3) Readings: LEL- 4%, O2- 12% VOC- 895 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**002- C1-P20 Lower Dome Quadrant B:**

This area was chosen because of its relation to 18" issue / receipt lines exiting the tank to lower level. Sounding located a hollow spot.

- 1) Course C1 Plate 20
- 2) Dry / no liquid (1/8" clearance behind plate)
- 3) Readings: LEL- 8%, O2- 7% VOC- 963 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm



**003- C2-P42 Lower Dome Quadrant C:**

This area was chosen because of its position in the tank and sounding located a hollow spot.

- 1) Course C2 Plate 42
- 2) Dry / no liquid (1/8" clearance behind plate)
- 3) Readings: LEL- 7%, O2- 9% VOC- 907 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**004- C3-P60 Lower Dome Quadrant D:**

This area was chosen because of its position in the tank and sounding located a hollow spot.

- 1) Course C3 Plate 60
- 2) Dry / no liquid (3/4" clearance behind plate)
- 3) Readings: LEL- 6%, O2- 13% VOC- 748 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**005- R8-P12 Barrel Quadrant C/D:**

This area was chosen because of its position in the tank, sounding located a hollow spot, plate bulging and relation to previous repair WP403.

- 1) Course 8 Plate 12
- 2) Dry / no liquid (1/8" clearance behind plate)
- 3) Readings: LEL- 7%, O2- 14% VOC- 813 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**006- R26-P15 Barrel Quadrant D:**

This area was chosen because of its position in the tank; sounding located a hollow spot, and relation to previous repairs WP383, WP379, and WP381.

- 1) Course 26 Plate 15
- 2) Dry / no liquid (1/4" clearance behind plate)
- 3) Readings: LEL- 5%, O2- 11% VOC- 827 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**007- E2-P16 Extension Ring Quadrant D:**

This area was chosen because of its position in the tank; sounding located a hollow spot, and relation to previous repairs WP076, WP077, and WP078.

- 1) Course E2 Plate 16
- 2) Dry / no liquid (3/4" clearance behind plate)
- 3) Readings: LEL- 9%, O2- 12% VOC- 984 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**008- E4-P13 Extension Ring Quadrant C/D:**

This area was chosen because of its position in the tank, sounding located a hollow spot, and growth out of WP075.

- 1) Course E4 Plate 13
- 2) Dry / no liquid (1/16" clearance behind plate)
- 3) Readings: LEL- 0%, O2- 19% VOC- 40 ppm
- 4) Mist of dust & moisture- volume not relevant or collectable
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**009- A-P68 Upper Dome Quadrant D:**

This area was chosen because of previously failed LT which indicated the possible presence of fuel.

- 1) Course A Plate 68
- 2) Dry / no liquid (1/16" clearance behind plate)
- 3) Readings: LEL- 2%, O2- 18% VOC- 300 ppm
- 4) Mist of dust & moisture- volume not relevant or collectable
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**010- R3-P3 Barrel Quadrant A:**

This area was chosen because of its position in the tank, sounding located a hollow spot, and relation to previous repairs.

- 1) Course 3 Plate 3
- 2) Dry / no liquid (1/16" clearance behind plate)
- 3) Readings: LEL- 7%, O2- 13% VOC- 780 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 0 ppm

**011- R11-P6 Barrel Quadrant B:**

This area was chosen because of previous failed LT and repair plate (WP301) had been removed.

- 1) Course 11 Plate 6
- 2) Dry / no liquid (1/16" clearance behind plate)
- 3) Readings: LEL- 6%, O2- 11% VOC- 800 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 400 ppm

**012- E3-P6 Extension Ring Quadrant B:**

This area was chosen because of its position in the tank, sounding located a hollow spot, plate bulging and relation to previous repair.

- 1) Course 11 Plate 6
- 2) Dry / no liquid (1/8" clearance behind plate)
- 3) Readings: LEL- 9%, O2- 7% VOC- 1000 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 39 ppm

**013- E2-P13 Extension Ring Quadrant A:**

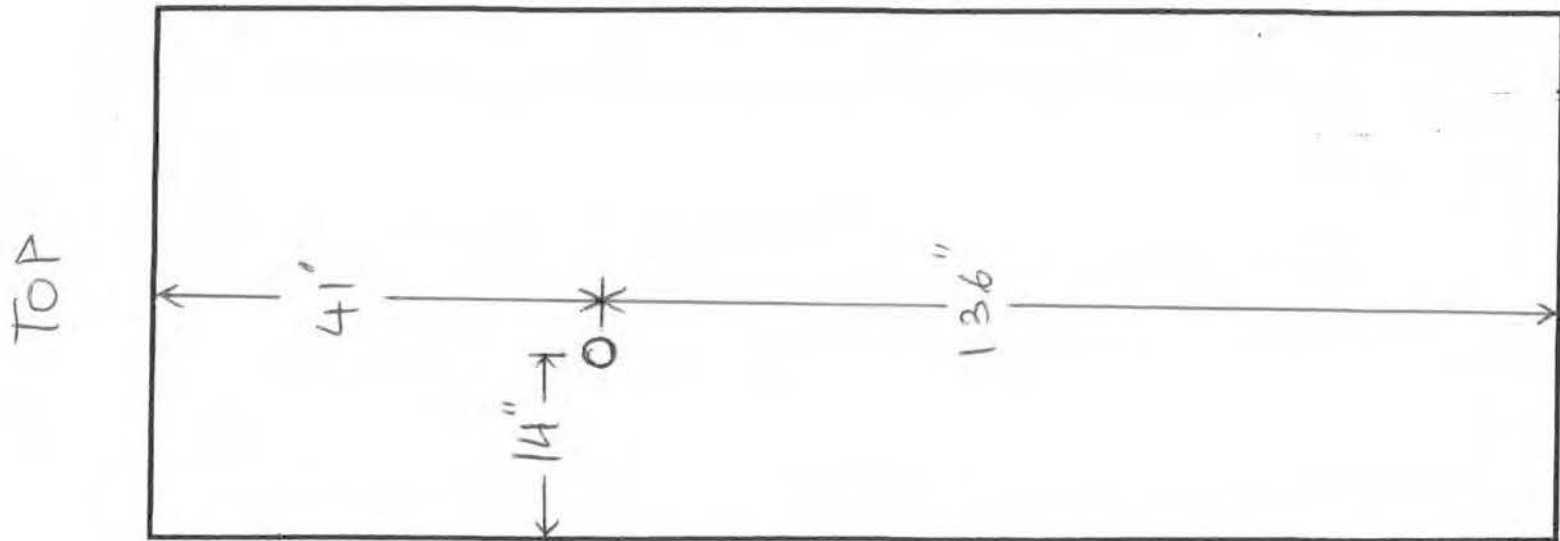
This area was chosen because of its position in the tank, sounding located a hollow spot and relation to previous repair.

- 1) Course E2 Plate 3
- 2) Dry / no liquid (1/4" clearance behind plate)
- 3) Readings: LEL- 4%, O2- 16% VOC- 850 ppm
- 4) Dry / no liquid
- 5) Readings: LEL- 0%, O2- 20.9% VOC- 37 ppm



# Willbros Government Services

Location:	Red Hill - Tank 5 WW
Location:	Free Product Reclamation Test Ports
Description:	Tank # 5 Row or Course - LOWER DOME C1 Sheet No - 001 Plate 2

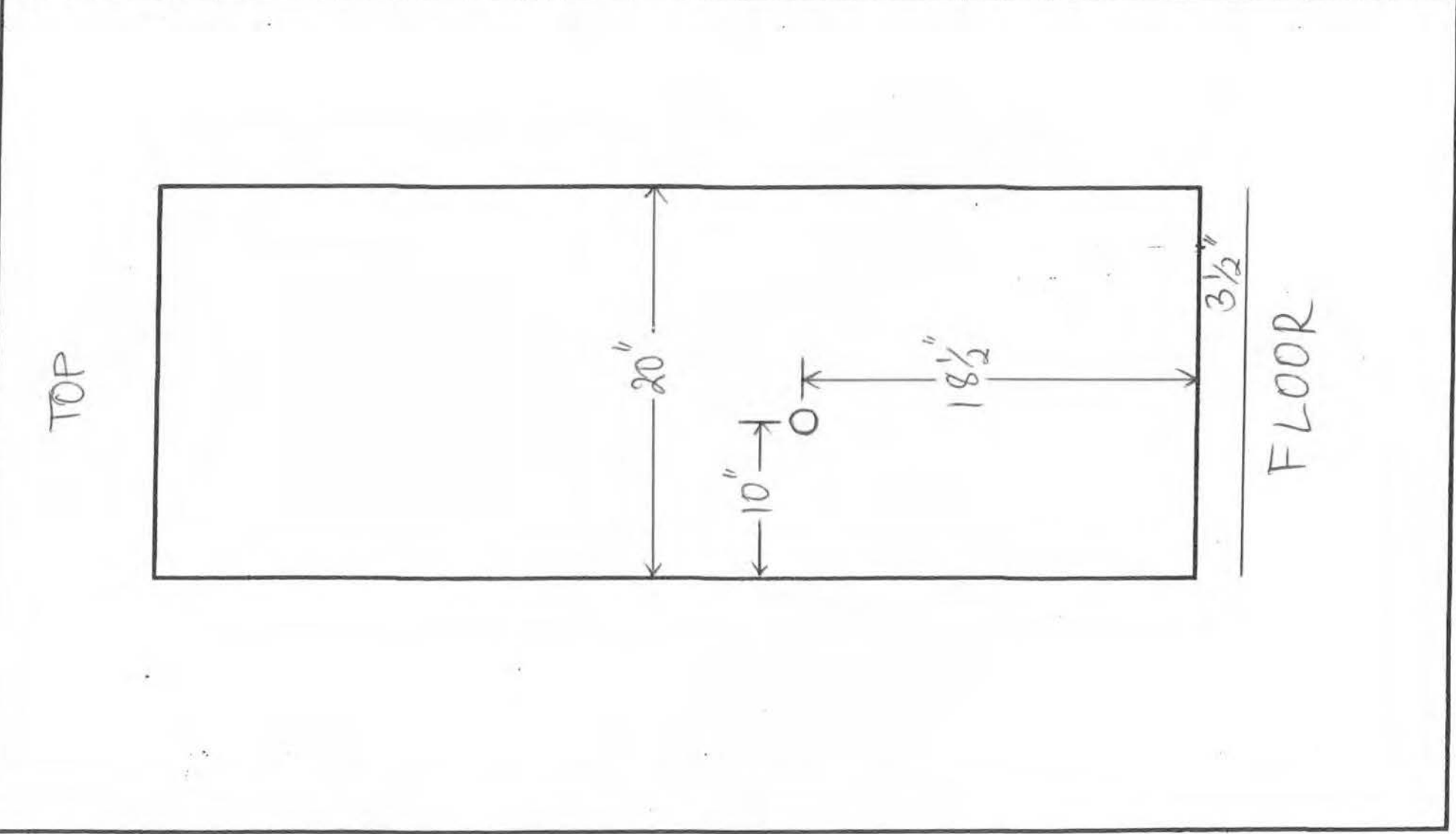






# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - LOWER DOME C1	Sheet No - 002 Plate 20

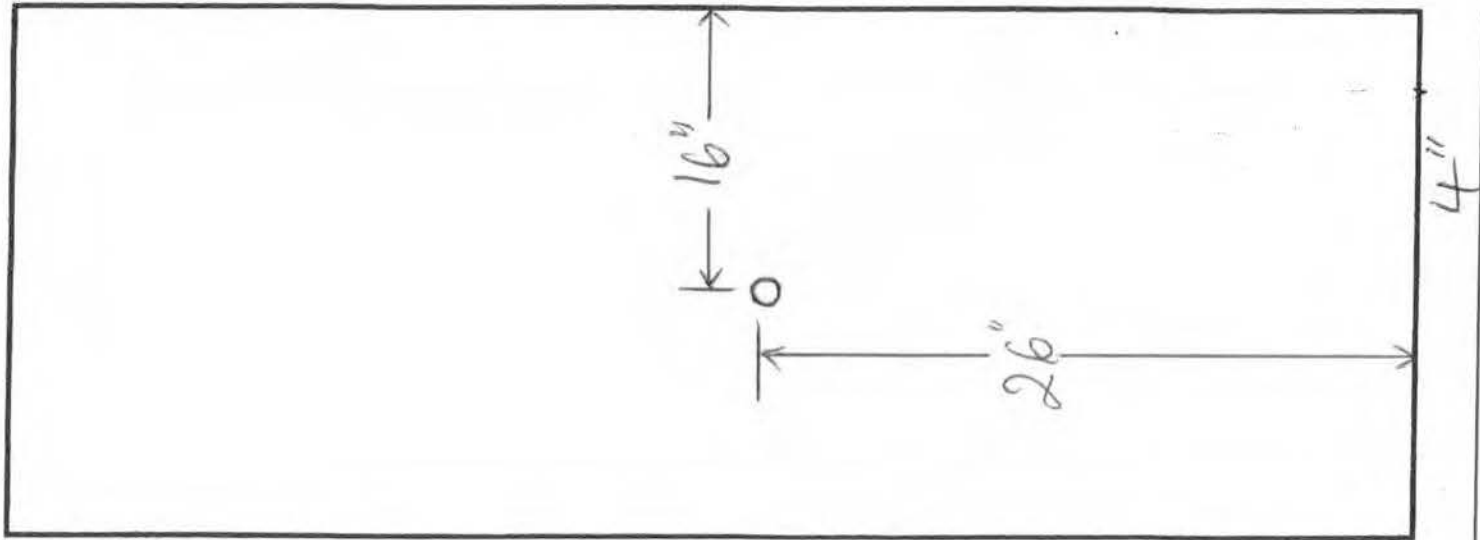




# Willbros Government Services

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Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - 4D C2	Sheet No - 003 Plate 42

TOP



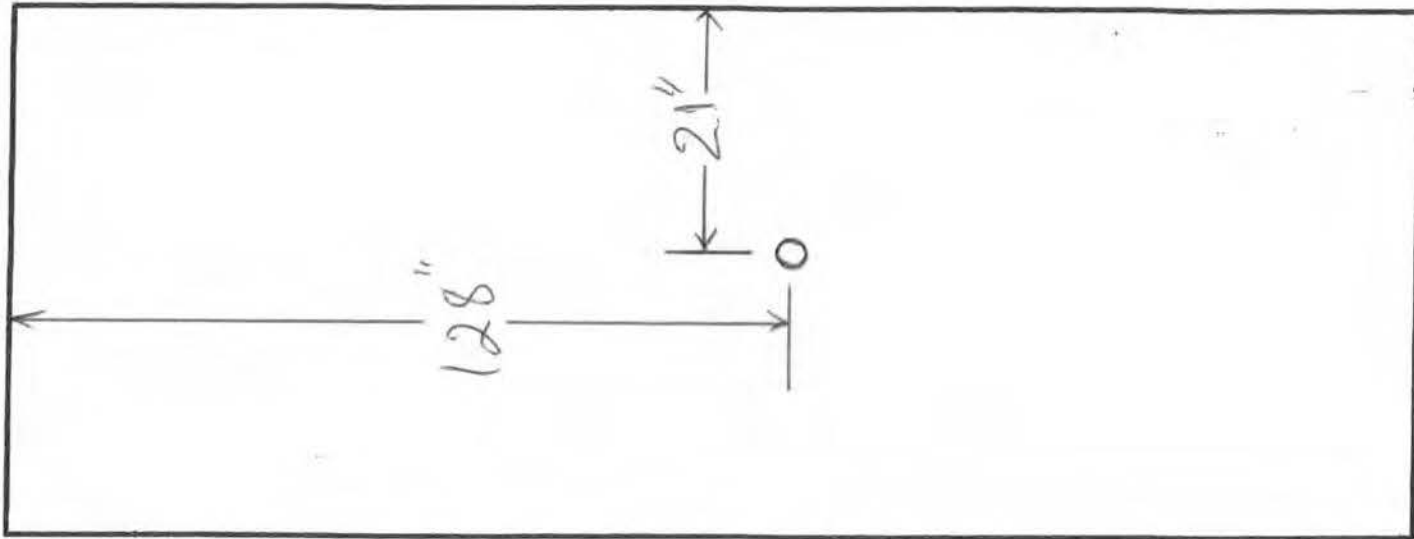
C1



# Willbros Government Services

Location:	Red Hill - Tank 5 WW
Location:	Free Product Reclamation Test Ports
Description:	Tank # 5 Row or Course - LOWER DOME C3 Sheet No - 004 Plate 60

TOP

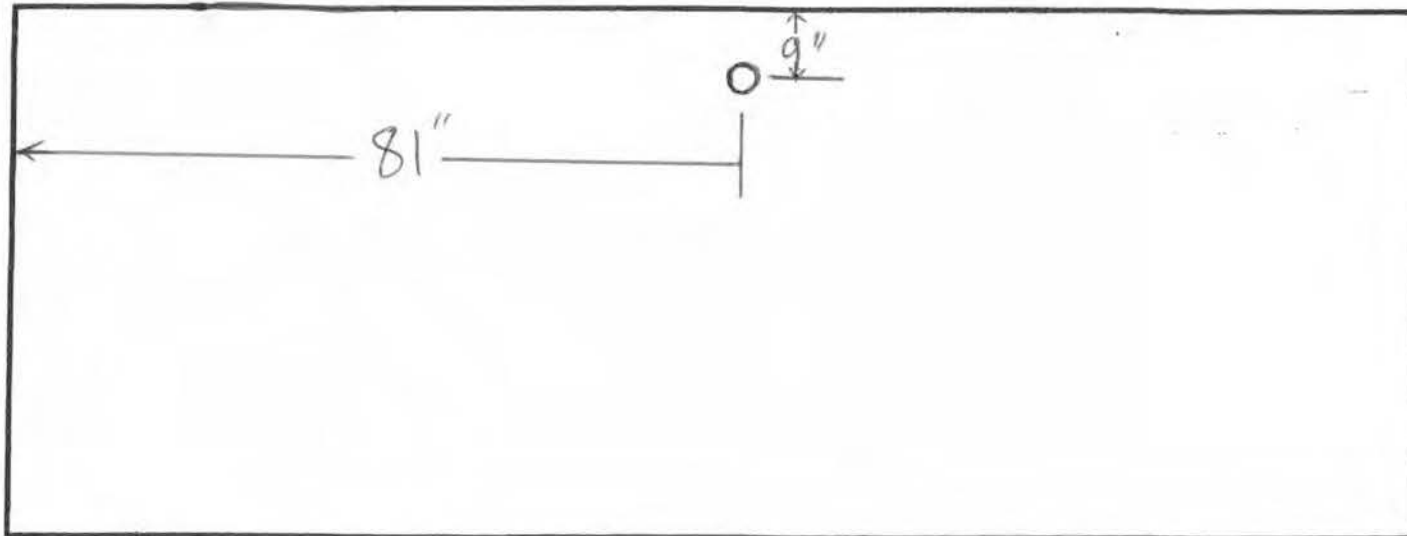




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - # 8	Sheet No - 005 Plate 12

TOP

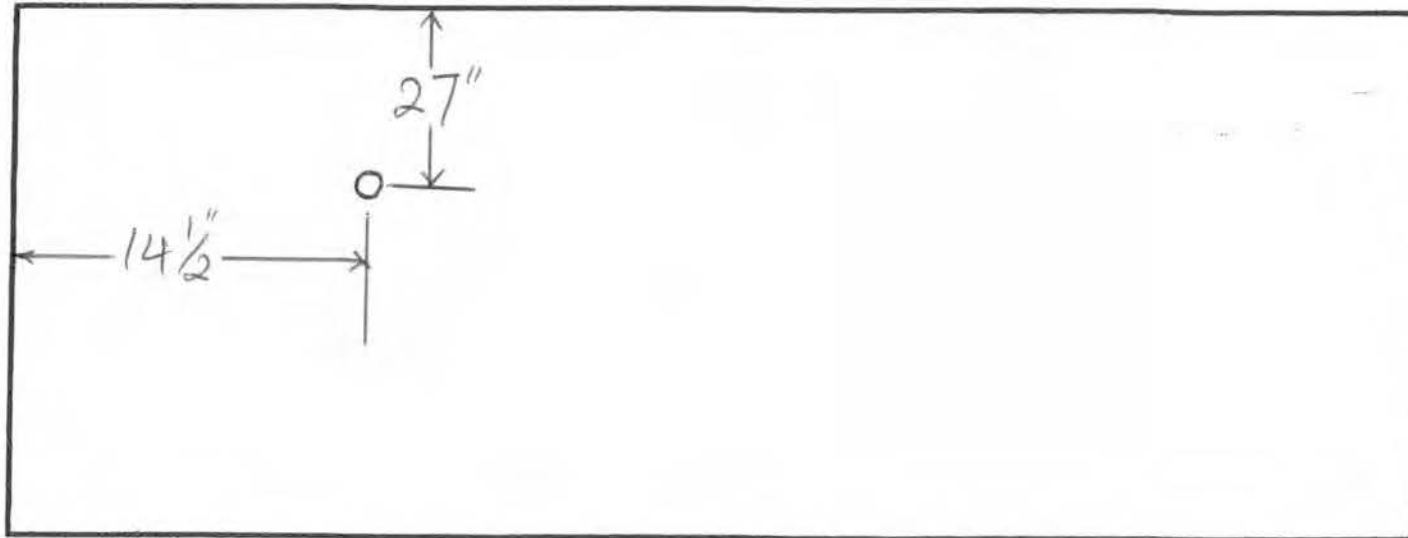




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - # 26	Sheet No - 006 Plate 15

TOP



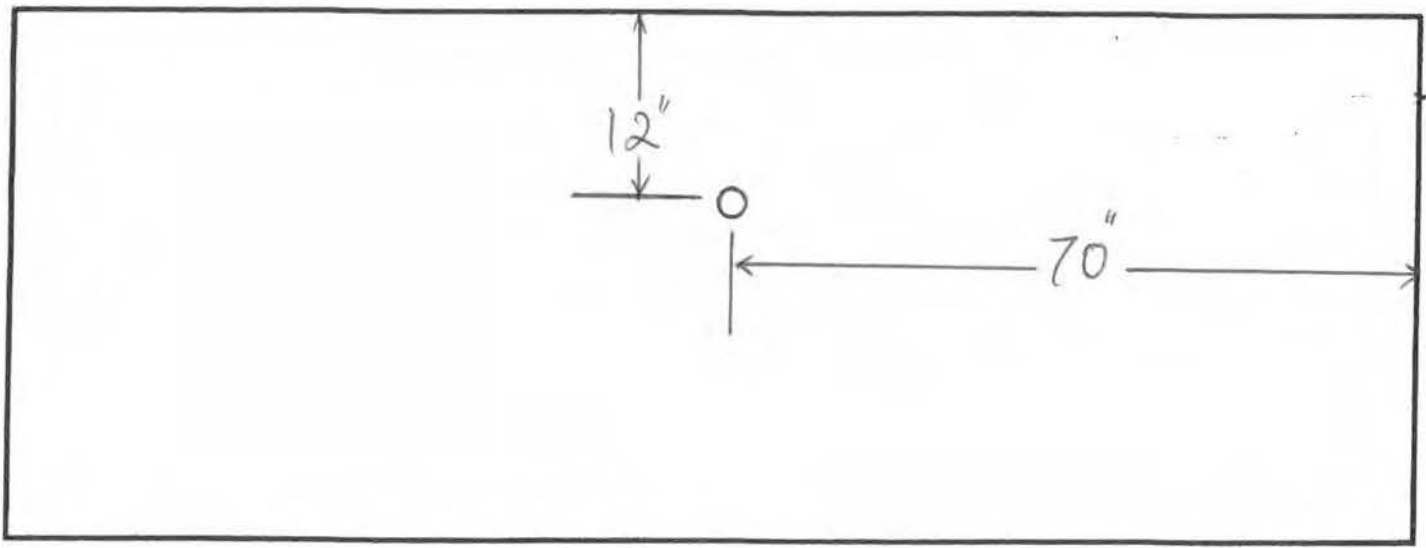




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - E2	Sheet No - 007 Plate 16

TOP

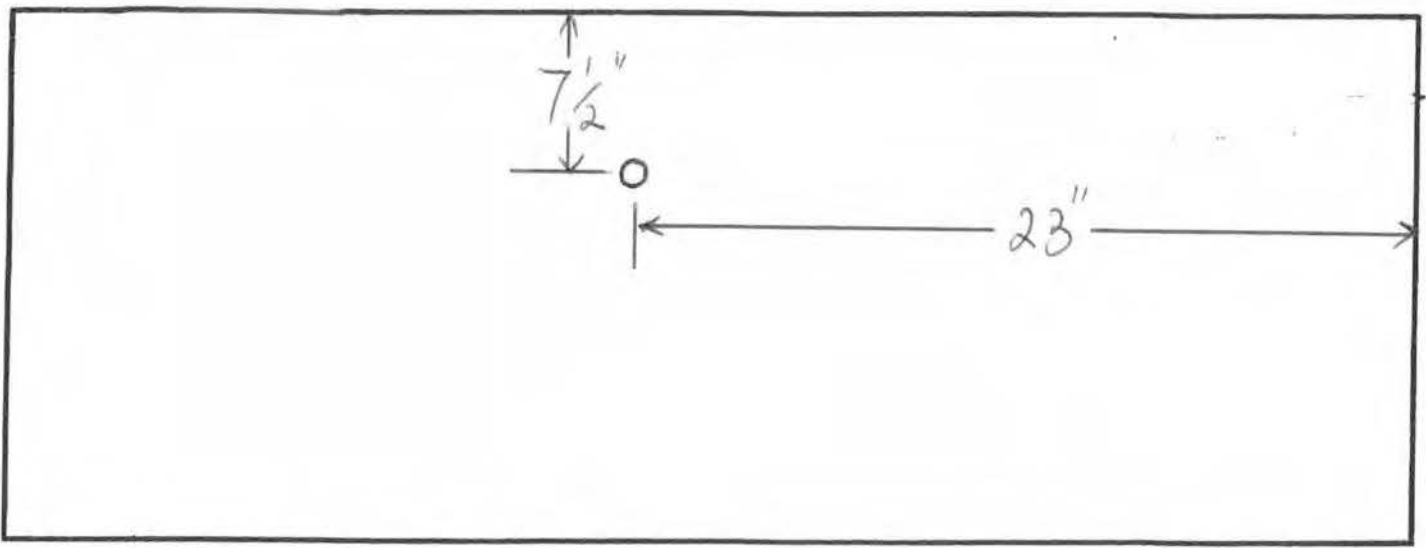




# Willbros Government Services

Location:	Red Hill - Tank 5WW		
Location:	Free Product Reclamation Test Parts		
Description:	Tank # 5	Row or Course - E 4	Sheet No - 008 Plate 13

TOP

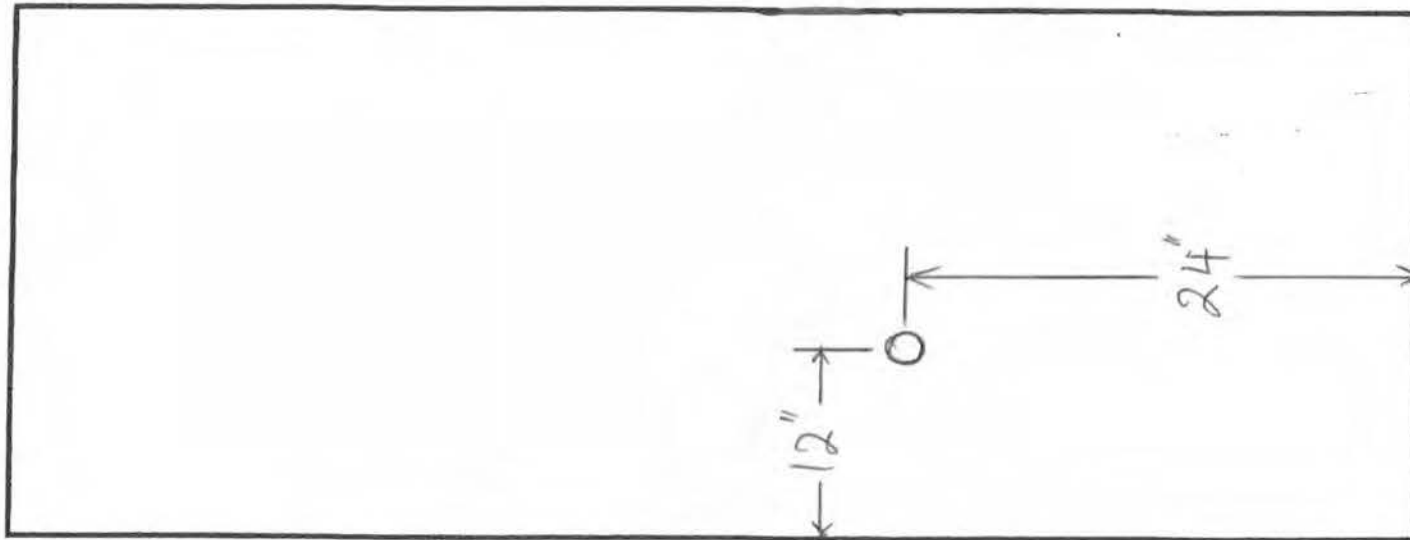




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - A	Sheet No - 009 Plate 68

TOP

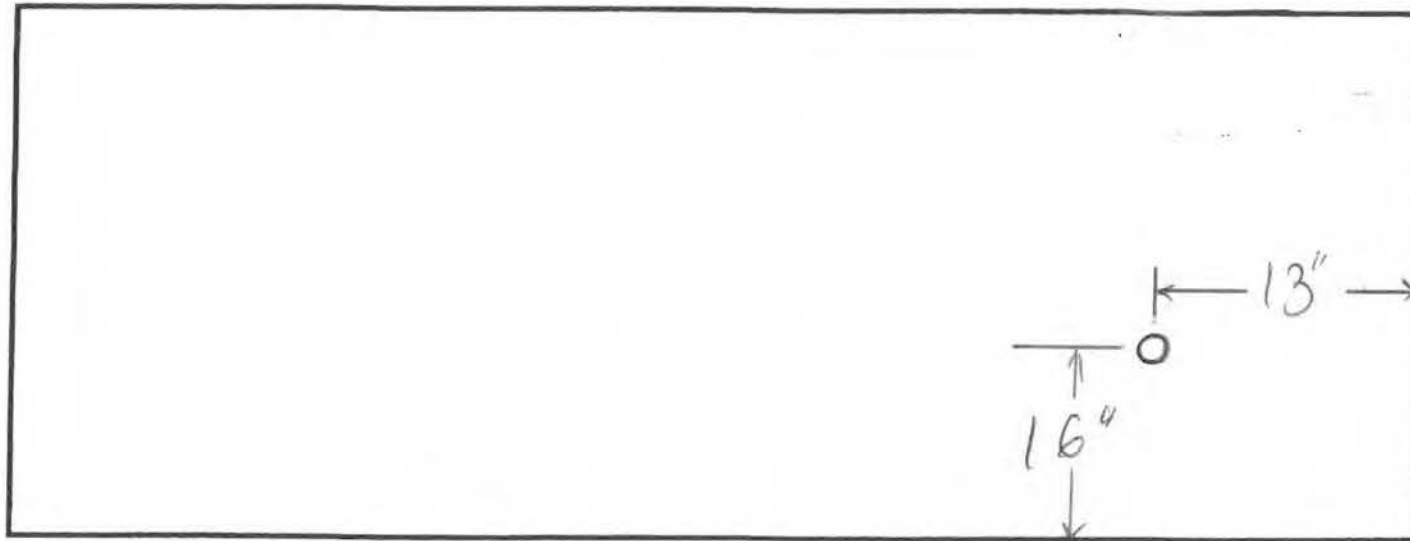




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - # 3	Sheet No - 010 Plate 3

TOP

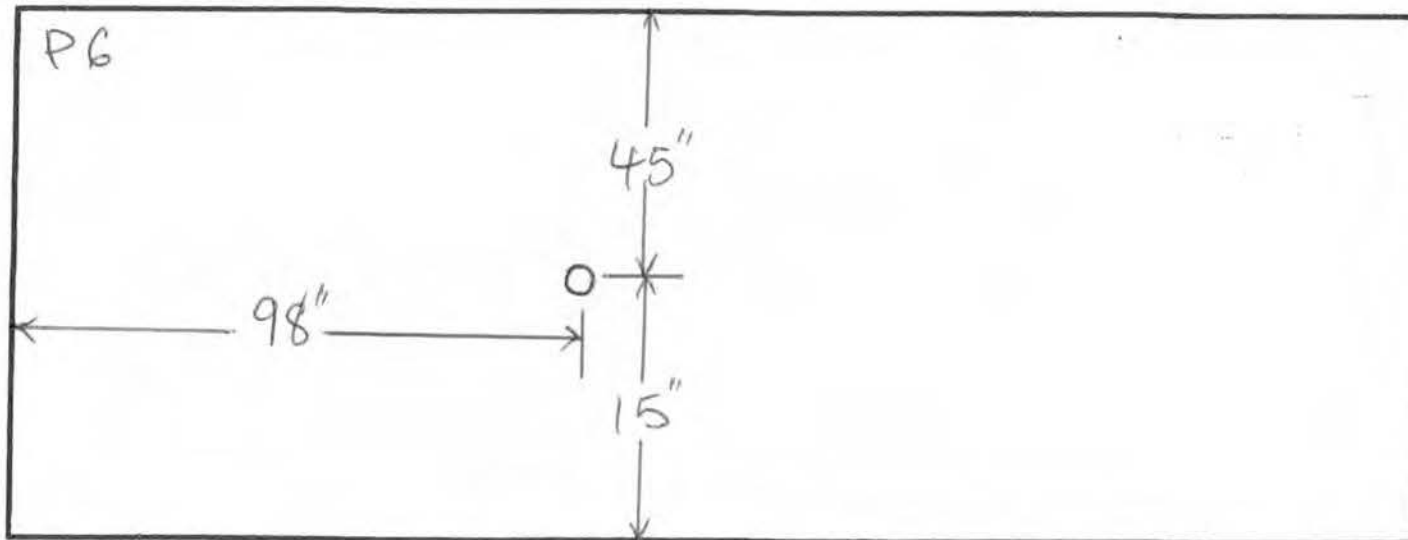




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - 3 11	Sheet No - 011 Plate 6

TOP



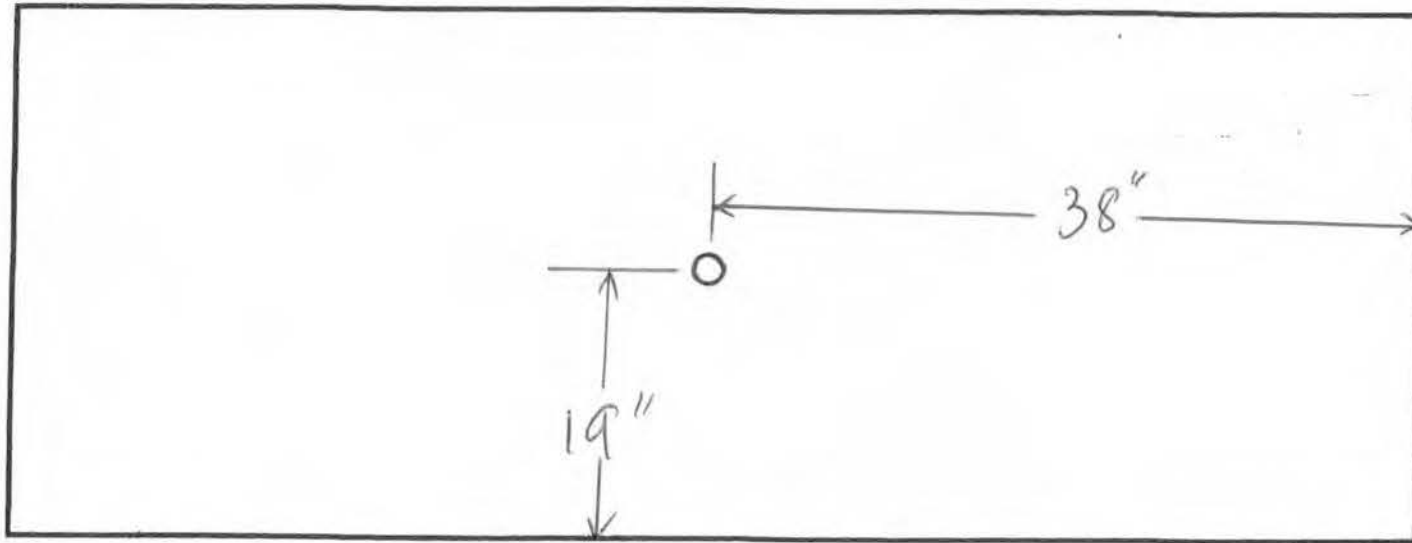




# Willbros Government Services

Location:	Red Hill - Tank 5 WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - E3	Sheet No - 012 Plate 6

TOP

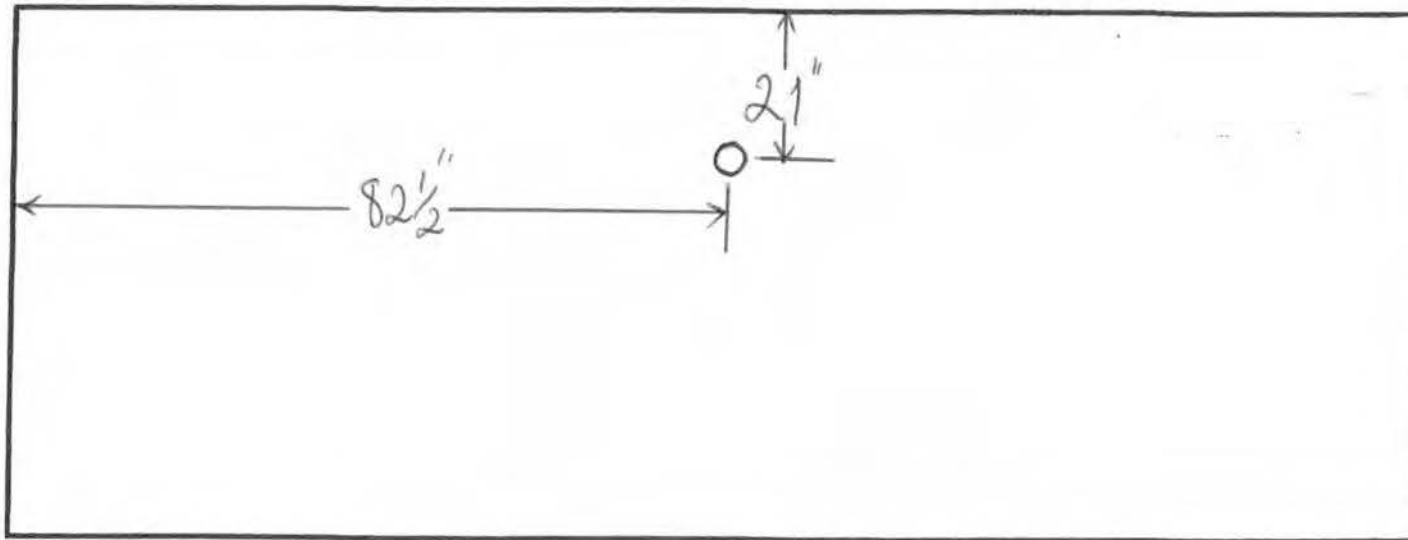




# Willbros Government Services

Location:	Red Hill - Tank 5WW		
Location:	Free Product Reclamation Test Ports		
Description:	Tank # 5	Row or Course - E2	Sheet No - 013 Plate 3

TOP





## Potential Free Product Reclamation Photo's

TASK ORDER #:	N 62583-09-D-0132/003	PROJECT TITLE:	CLEAN, INSPECT & REPAIR TANKS 5 & 17 RED HILL COMPLEX
WGS PROJECT #:	54118 WW	DATE:	OCTOBER 28 & 29, 2014

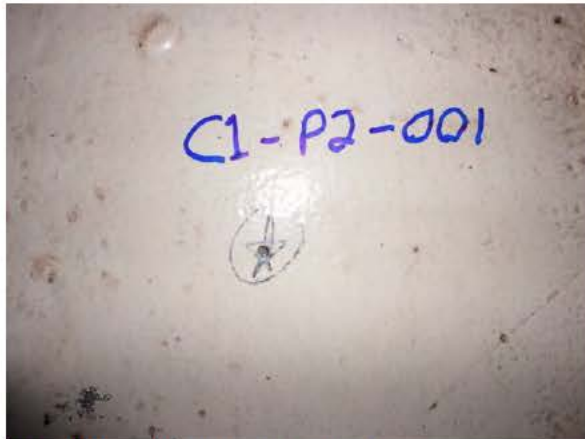
### SITE PHOTOGRAPHS



Port 001- C1 Plate 2; Located



Port 001- C1 Plate 2; Vacuumed



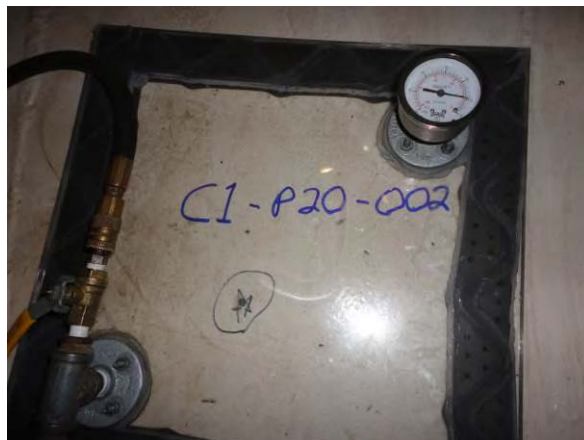
Port 001- C1 Plate 2; Drilled



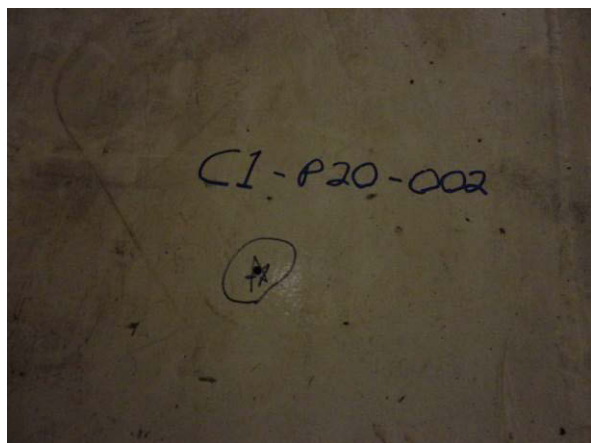
Port 001- C1 Plate 2; Air Monitoring



Port 002- C1 Plate 20; Located



Port 002- C1 Plate 20; Vacuumed



Port 002- C1 Plate 20; Drilled



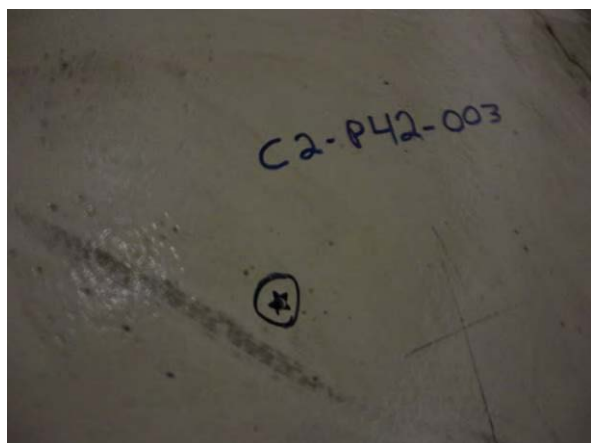
Port 002- C1 Plate 20; Air Monitoring



Port 003- C2 Plate 42; Located



Port 003- C2 Plate 42; Vacuumed

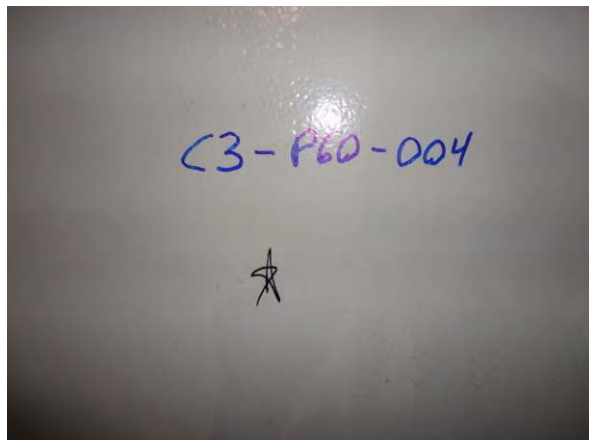


Port 003- C2 Plate 42; Drilled



Port 003- C2 Plate 42; Air Monitoring

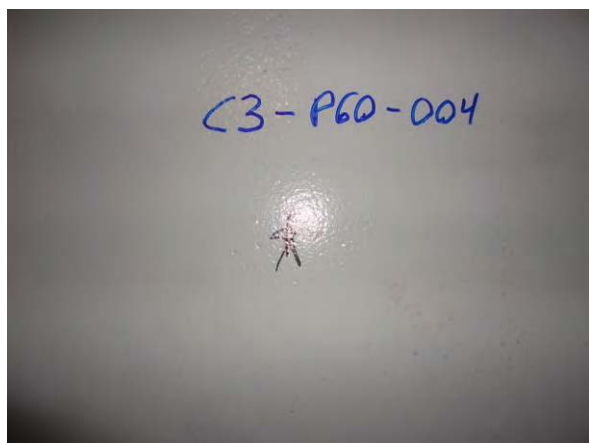




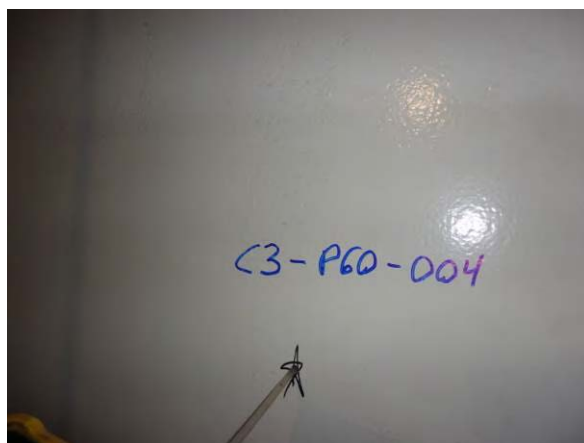
Port 004- C3 Plate 60; Located



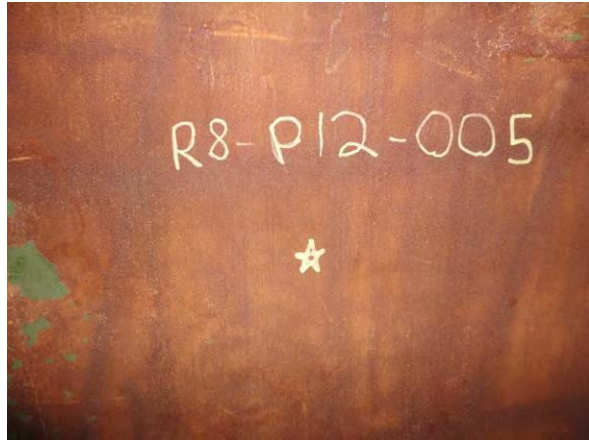
Port 004- C3 Plate 60; Vacuumed



Port 004- C3 Plate 60; Drilled



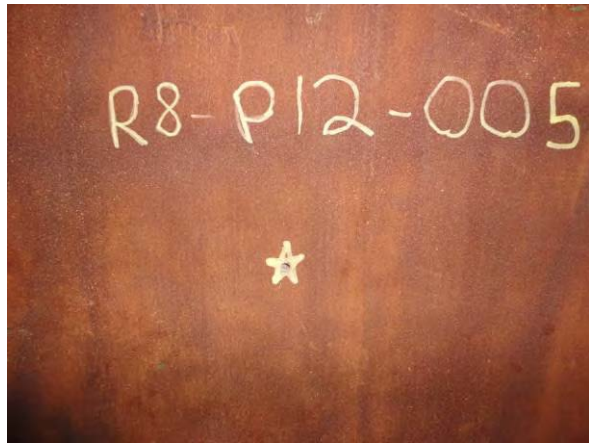
Port 004- C3 Plate 60; Air Monitoring



Port 005- R8 Plate 12; Located



Port 006- R26 Plate 15; Located



Port 005- R8 Plate 12; Drilled



Port 006- R26 Plate 15; Drilled



Port 005- R8 Plate 12; Vacuumed

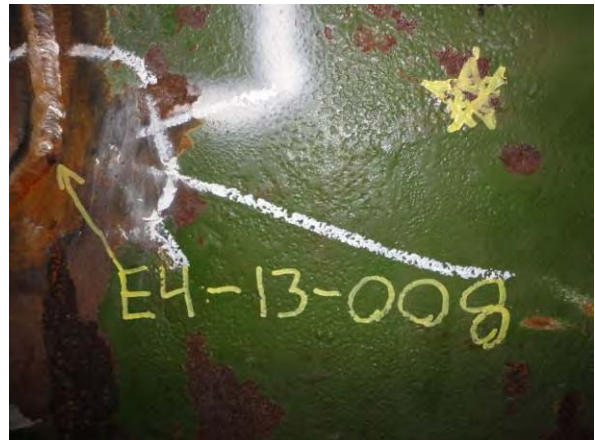


Port 006- R26 Plate 15; Vacuumed

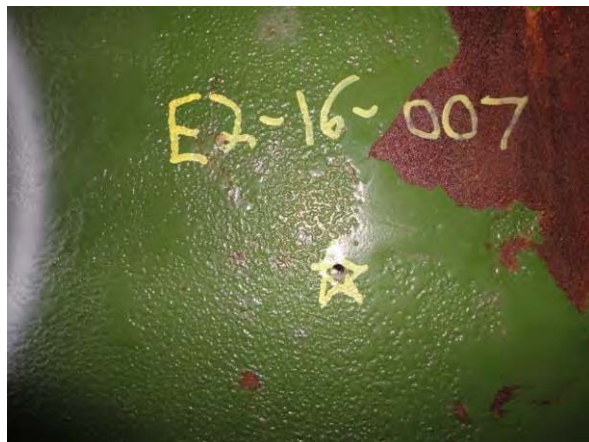




Port 007- E2 Plate 16; Located



Port 008- E4 Plate 13; Located



Port 007- E2 Plate 16; Drilled



Port 008- E4 Plate 13; Drilled



Port 007- E2 Plate 16; Vacuumed



Port 008- E4 Plate 13; Vacuumed



Port 009- A Plate 68; Located



Port 010- R3 Plate 3; Located



Port 009- A Plate 68; Drilled



Port 010- R3 Plate 3; Drilled



Port 009- A Plate 68; Vacuumed



Port 010- R3 Plate 3; Vacuumed





Port 011- R11 Plate 6; Located



Port 012- E3 Plate 6; Located



Port 011- R11 Plate 6; Under WP301



Port 012- E3 Plate 6; Drilled

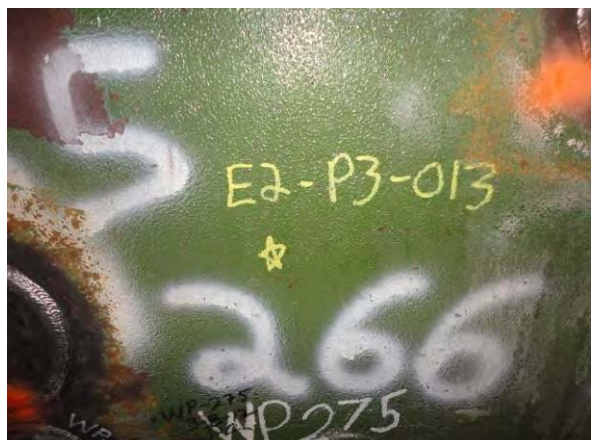


Port 011- R11 Plate 6; Vacuumed

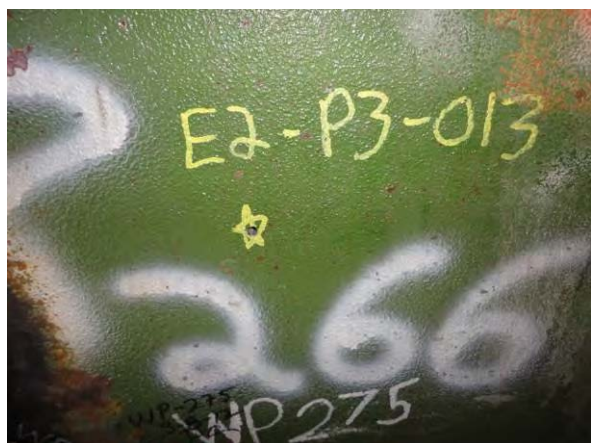


Port 012- E3 Plate 6; Vacuumed

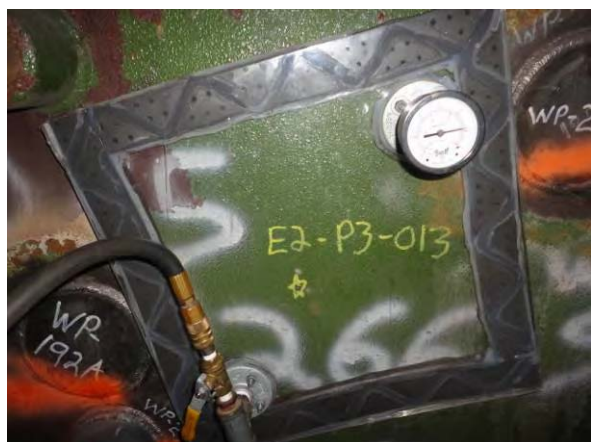




Port 013- E2 Plate 3; Located



Port 013- E2 Plate 3; Drilled



Port 013- E2 Plate 3; Vacuumed



WILLBROS GOVERNMENT SERVICES (U.S.), LLC

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## PRESSURE TEST PROCEDURE NDT-3

Revision 9 June 5, 2014

Rev	Description	Reviewed	Approved
0	Approved	IQC	DG
1	General	IQC	DG
2	General	IQC	DG
3	General	IQC	DG
4	General	IQC	DG
5	General	IQC	DG
6	General	IQC	TDA
7	General	IQC	RGG
8	General	IQC	RGG
9	General	IQC	RGG

## TABLE OF CONTENTS

- I. Scope
- II. Responsibility
- III. Requirements
- IV. Procedure
- V. Calibrations
- VI. Records

# HYDROSTATIC TEST PROCEDURE

## I. SCOPE:

This procedure is to insure that all the requirements of the applicable sections of the ASME Code are met and to insure the safety of all personnel which are involved in performing the hydrostatic test.

## II. RESPONSIBILITIES:

The Site Manager or Field Superintendent is responsible for the safe performance of the hydrostatic test. Only trained personnel, aware of these procedural steps, shall be used to conduct the test.

The Quality Control Manager or his designee is responsible for witnessing and documenting the results of the hydrostatic test and assuring that it is performed safely in accordance with this procedure.

For hydrostatic tests performed to meet ASME Code requirements, the Quality Control Manager or his designee is responsible for notifying the Authorized Inspector in advance of the test so that he may be present.

NOTE: The Authorized Inspector must witness and accept all hydrostatic test performed to meet Code requirements.

## III. REQUIREMENTS:

All welds shall be satisfactorily completed and the vessel and or piping released by Quality Control for hydrostatic testing.

NOTE: All fabrication shall have been completed, except for operations which cannot be performed prior to the test such as weld end preparation, seal welding of vent plugs or cosmetic grinding on the base material which does not affect the required thickness. All examinations shall have been performed, except those required after the test.

## IV. PROCEDURE:

- 1.0 The hydrostatic test pressure will be 162 PSI. This number is based on the maximum pressure a tank full of water will produce on the piping. The formula  $PSI_{max} = 1.5((0.433 \times Sp \text{ Gr})(H))$  was used to determine the final pressure. The height was assumed at 250 ft and the Specific Gravity at 1.  $162 = 1.5((0.433 \times 1)(250))$ .

- 2.0 Flanges and nozzles which are not utilized during the hydrostatic test shall be blanked and plugged using material approved for the job or standard approved material in the hydrostatic test area.
  - 2.1 Material (blinds, threaded plugs, bolting, etc.) shall be compatible for the design pressure of the vessel and or piping and for use with the specified test pressure. Only material in good physical condition shall be used.
  - 2.2 Material used for welded closures shall be as specified on the vessel/piping drawing and identified by "P" number or by material specification.
  - 2.3 Welded connections made to temporary closures shall have the minimum weld sizes as specified on the vessel/piping drawing.
  - 2.4 Any additional NDE specified on the drawing for welded temporary closure shall be performed and any necessary repairs made.
  - 2.5 These connections must be visually inspected for verification of proper material, preparation, welding, threading, or bolting as specified on the vessel/piping drawing.
  - 2.6 The design and capacity of test plugs will be verified by Supervision and Quality Control. The plugs will be secured by chain or other means to assure containment if they slip.
  - 2.7 Visual inspection by Quality Control of all closures is required before pressure application.
- 3.0 Hydro Trees will be engineered and constructed to WGS Engineering specifications or better. All Hydro Trees will be marked with their rated capacity. Temporary drains and vents will use the same or higher schedule pipe as the Hydro Tree.
- 4.0 The testing medium shall be clear city tap water with less than 50 ppm Chloride content unless otherwise specified in the vessel/piping design specifications. This report will include the latest city water quality report. Other liquid mediums may be used if there is a danger of freezing or water would cause adverse effects on the vessel/piping. After testing is completed, the water will be drained into totes for disposal off-site.
- 5.0 A calibrated gauge shall be selected with a dial range of at least 1 1/2 times and not more than 4 times the hydrostatic test pressure. The increments between graduations will be 1 psig or less such that the Quality Control Inspector and the operator controlling the test shall be able to determine when the required test pressure has been applied.

- 5.1 Digital reading pressure gauges having a wider range of pressure may be used provided the readings give the same or greater degree of accuracy as obtained with dial pressure gauges.
- 5.2 The indicating gauge shall be mounted inside the tank and directly to the piping as near as practical on the top most part undergoing the hydrostatic test. Hydrostatic head on the gauge shall be considered depending on the location of the gauge.
- 5.3 The indicating gauge will be readily visible to the operator controlling the pressure applied. For large vessels, consideration shall be given to the use of a recording gauge in addition to indicating gauges.
- 5.4 Using a thermocouple, we will measure temperature to 0.1°F, throughout the test.
- 5.5 A pressure chart recorder will be used to continuously plot pressure over the duration of the entire test.
- 5.6 The official pressure sensing device will be a deadweight tester capable of measuring in at least 1 psi increments.
- 6.0 Connect all fill and vent connections as necessary.
  - 6.1 Open vents must be located at the high point of the vessel/piping during the fill up to purge the air from the system.
  - 6.2 A hose or some other means to control water release should be installed on the high point vent.
- 7.0 Prior to filling the vessel, all personnel not involved with the hydrostatic test shall be kept at a safe distance from the testing area. The item to be hydro tested, the pump and the high pressure hose will be roped off at a safe distance with red barricade tape.
- 8.0 The temperature of the testing medium shall be as specified in the vessel / piping design specifications.
  - 8.1 The testing medium shall be at least ambient temperature but in no case less than 70 degrees F for Section I items. For NBIC repairs, the metal temperature should not be less than 60 degrees F preferably at least 30 degrees above the MDMT but not more than 120 degrees F for section VIII Division 1 items. The temperature for B31.3 Piping is limited by the stress value at test pressure-temperature.
  - 8.2 The test pressure shall not be applied until the vessel and its contents are at about the same temperature.
- 9.0 The vessel shall be filled with the testing medium until all air pockets have been expelled. The vent valve shall be closed when it is determined that venting is completed.



9.1 Vents shall be provided at all high points of the vessel/piping in the position in which it is to be tested to purge possible air pockets while the vessel is filling. If the operator or the Quality Control Inspector determines the vent arrangement is inadequate, the test shall be aborted until the problem is resolved.

CAUTION: The venting of air at ALL high points must be checked IMMEDIATELY prior to the pressure test. As the temperature of the testing medium increases, air may be released. It must be vented.

9.2 If the pressure does not come up readily when pumping, stop. This could be an indication of air in the system. Depressurize and re-purge to assure the removal of air.

10.0 The operator of the hydrostatic pump shall have a clear view of the test pressure gauge, so that he will be aware of the test pressure at all times.

10.1 The pump operator will be stationed away from the immediate vicinity of the vessel/piping being tested as deemed necessary to provide for his safety. A means of observing the pressure gauge will be provided.

10.2 If the operator or the Quality Control Inspector suspects any gauge to be in error, the test will be aborted until such gauge has been replaced or recalibrated.

11.0 At this time and until the conclusion of the hydrostatic test, the pump operator will not leave the pump station for any purpose except when relieved by an individual competent in the performance of this operation.

12.0 The hydrostatic pressure shall be applied gradually until the required test pressure of 162 psig is reached. The pressure application will be witnessed by the Quality Control Inspector. A close visual inspection WILL NOT BE conducted at this time.

12.1 The test pressure shall never be more than 170 psig.

12.2 NO FITTINGS OR CONNECTIONS WILL BE TIGHTENED WHILE THE SYSTEM OR VESSEL IS UNDER PRESSURE.

12.3 If a leak is detected during testing, the pressure is to be removed prior to approaching the vessel.

12.3.1 Leakage of temporary gaskets or plugs installed for the purpose of conducting the hydrostatic test and which will be replaced later may be permitted unless the leakage exceeds the ability to maintain the vessel/ piping test pressure for the required amount of time or interferes with the evaluation of the test results.

13.0 Once the line is pressurized to 162 psig, that pressure will be maintained for 4 hours.

- 13.1 The holding time shall be a minimum of four (4) hours or a greater time if specified on the vessel/piping drawing or requested by the Inspector to complete the visual inspection of joints or components.
- 14.0 A close visual examination will then be conducted of all joints and connections at this time. Since some of the piping is not accessible for visual inspection DV/DP calculations will be performed. There will be two (2) DV/DP values. One DV/DP value will be theoretically calculated using the ambient temperature within the tank. The other DV/DP value will be read from actual field measurements. If the calculated and measured DV/DP values are within the limits specified by the California State Fire Marshal's Office, the tested section of piping will be determined acceptable (PASS).
- 15.0 Upon completion of the hydrostatic test, the pressure will be dropped. The pressure gauge will be checked to verify it has returned to zero.
- 16.0 Drain and vent valves will be opened to allow the vessel to drain. Never open the drains on a large vessel without first opening the vent. Open lines shall be elevated in order to be free of any standing water.

## V. Calibrations

The test gauge(s) shall be calibrated within a (1) year current time frame and in accordance with NIST standards. A copy of the gauge(s) calibration will be present during the test.

## VI. Records

The Hydrostatic/Pneumatic Pressure Test will be recorded on the appropriate form as determined by the QC Inspector at the completion of the test. The test record will be maintained for the duration as specified by the applicable code.

### 1.0 Approved Test Forms

- 1.1 Record of Hydrostatic/Pneumatic Test
- 1.2 Pressure Test Certificate

A copy of the test gauge calibration(s) shall be attached to the test report for final records. All test records or reports will be submitted in the project final report or data book.

Test data and results will be forwarded for review to NAVFAC EXWC within 24 hours of test completion. Forwarded test data and results will include a statement of PASS or FAIL and reasoning.

## Record of Hydrostatic / Pneumatic Test

Job Number \_\_\_\_\_ Location \_\_\_\_\_

Sheet Number \_\_\_\_\_ Mark Number \_\_\_\_\_

Date of Test \_\_\_\_\_ Gage Number \_\_\_\_\_ Calibration \_\_\_\_\_

Chart Recorder Number \_\_\_\_\_

Calibration Date \_\_\_\_\_

Hydrostatic Test Pressure \_\_\_\_\_ PSIG

Test Medium \_\_\_\_\_

Duration of Test \_\_\_\_\_

Witness and Accepted by:

Inspector: \_\_\_\_\_ Date: \_\_\_\_\_

Customer Representative \_\_\_\_\_ Date: \_\_\_\_\_



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## Pressure Test Certificate

PROJECT	LOCATION	JOB NUMBER
CONTRACTOR	P & ID No.	
SERVICE		
TEST PACK NUMBER.	DRAWING No.	
SYSTEM NUMBER		
MARK No.	ISO No.	
LINE No.		
LINE SPECIFICATION	TEST MEDIUM	
DESIGN PRESSURE (MAWP)	PSI	TEST PRESSURE PSI
STRESS RELIEVED      YES      NO	INTERNAL LINING      YES      NO	
ALL PRE- TEST NDE COMPLETE AND ACCEPTED	SIGNATURE	DATE
MATERIAL RECORDS COMPLETE	SIGNATURE	DATE
WELDING HISTORY RECORDS COMPLETE	SIGNATURE	DATE
PRE-TEST INSPECTION	FOREMAN SIGNATURE	DATE
WELDING OF PRESSURE PARTS COMPLETE	_____	SYSTEM FILLED AND PURGED OF AIR
PROPER GASKETS, BOLTS AND BLINDS	_____	TEMPERATURE WITHIN SPECIFICATION
TEMPORARY VENTS AND DRAINS INSPECTED	_____	HYDRO EQUIPMENT AND GAGES INSPECTED
TEST PLUGS INSPECTED AND SECURED	_____	OPERATORS PROPERLY INSTRUCTED
INSTUMENTATION BLOCKED OR REMOVED	_____	BARRACADES IN PLACE
VALVES IN THE RIGHT POSITION (OPEN/CLOSED)	_____	AREA CLEARED OF PERSONEL
TEST MEDIUM WITHIN SPECIFICATION	_____	_____
QUALITY CONTROL SIGNATURE		DATE
PRESSURE TEST	DATE OF TEST	AMBIENT
DURATION		TEMP.
START      FINISH		
COMMENTS (TO INCLUDE GAGE NUMBER AND CALIBRATION DATE)		
	Inspected by	Witnessed by
COMPANY		
SIGNATURE		
PRINT NAME		
DATE		
POST HYDRO RESTORATION		
HYDRO BLOWN DOWN & DRY	_____	CONTROL & CHECK VALVES INSTALLED
HYDRO BLINDS PULLED	_____	HIGH POINT PLUGS SEAL WELDED & INSPECTED
PROPER GASKETS INSTALLED	_____	NDE ON PLUG SEAL WELDS COMPLETE
PROPER BOLTING & TIGHTNESS	_____	DRAIN / VENT VALVES CLOSED & PLUGGED
	Inspected by	Witnessed by
COMPANY		
SIGNATURE		
PRINT NAME		
DATE		

STRESS CALCULATIONS FOR 3/4" SA106-GR B PIPE  
t-12.5% for pipe with no Corrosion Allowance

ASME PG-27.2.1 TUBING PRESSURE CALCS. <=5"OD

Thickness	Diameter	Stress	Exp tubes
0.135	1.05	17100	0
t	D	S	e

$$P = S [ 2t - 0.01D - 2e / D - ( t - 0.005D - e ) ]$$

Pressure	Sch 80
2218.725	

ASME PG-27.2.1 TUBING PRESSURE CALCS. <=5"OD

Thickness	Diameter	Stress	Exp tubes
0.192	1.05	17100	0
t	D	S	e

$$P = S [ 2t - 0.01D - 2e / D - ( t - 0.005D - e ) ]$$

Pressure	Sch 160
3193.425	

ASME PG-27.2.1 TUBING PRESSURE CALCS. <=5"OD

Thickness	Diameter	Stress	Exp tubes
0.269	1.05	17100	0
t	D	S	e

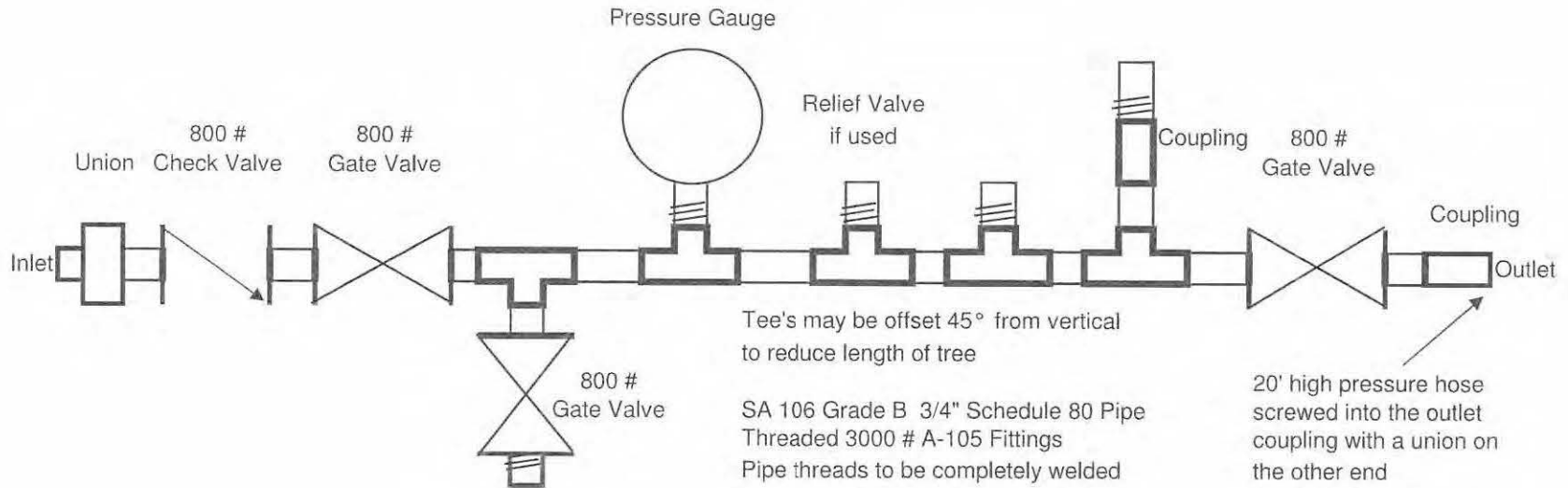
$$P = S [ 2t - 0.01D - 2e / D - ( t - 0.005D - e ) ]$$

Pressure	Sch XXS
4510.125	

MAWP FOR HYDRO TREE VALVES:

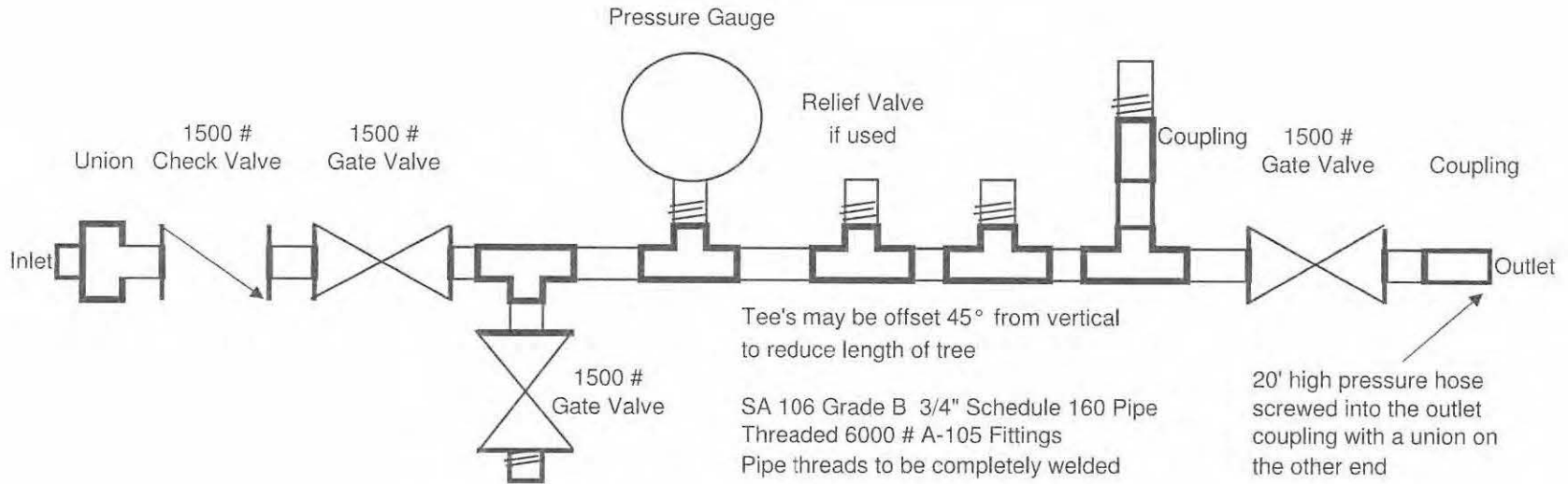
TYPE	PRESSURE
800#	2000#
1500#	3750#
2500#	6250#

## Hydro Tree Rated to 1500 PSI

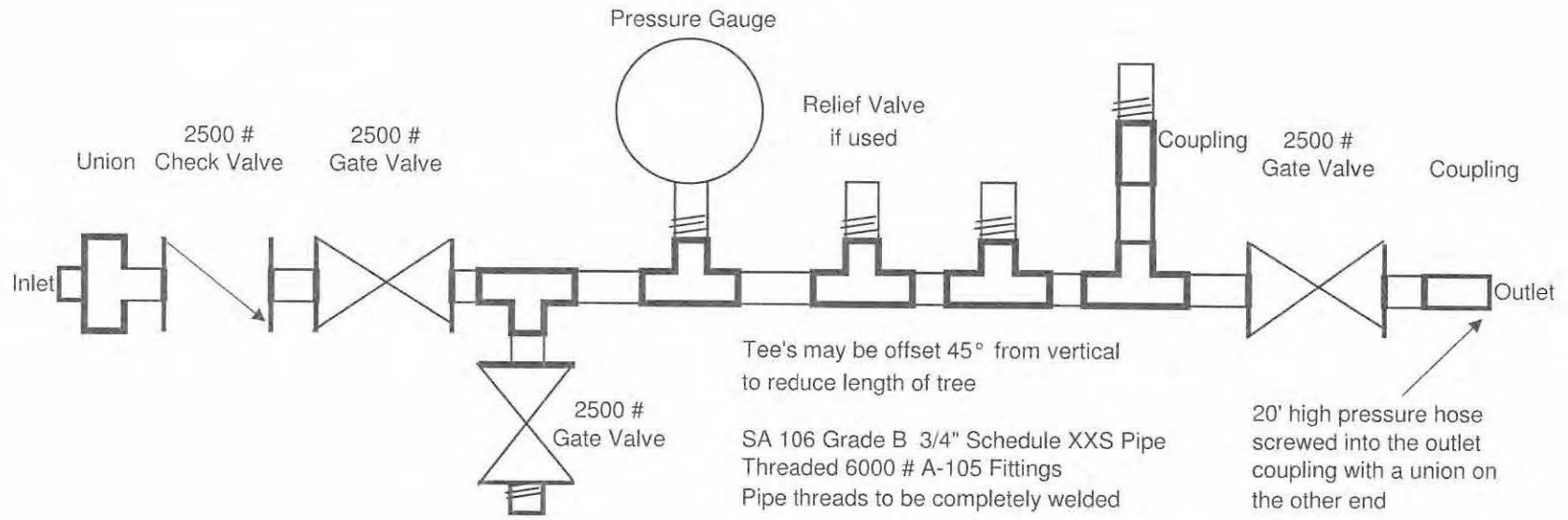




# Hydro Tree Rated to 3000 PSI



# Hydro Tree Rated to 4500 PSI



Tee's may be offset 45° from vertical to reduce length of tree

SA 106 Grade B 3/4" Schedule XXS Pipe  
Threaded 6000 # A-105 Fittings  
Pipe threads to be completely welded

20' high pressure hose  
screwed into the outlet  
coupling with a union on  
the other end



## 1. WILLBROS CONCLUSIONS AND RECOMMENDATIONS

The preliminary report completed by Pipeline Petroleum Services, Inc. and issued to the Navy concluded that the both the 18-inch and 32-inch lines for Tank-5 at Red Hill passed the contract required volume correction calculations as set forth by the California State Fire Marshal's office. Pipeline Petroleum Services stated that the entire test was considered inconclusive in their opinion because each test failed the temperature – pressure evaluation and their thoughts were that there is trapped air into the system and that is why the system failed the temperature – pressure evaluation.

During Willbros review of the report prepared by Pipeline Petroleum Services, it was noted that during testing, the temperature probe in the tunnel recorded a 0.1 °F drop in temperature and the temperature probe in the tank recorded a 2.0 °F rise in temperature.

James Hagen the Project Manager for the Red Hill Tank-5 work informed us that there can easily be a 2.0 °F temperature change in the tank from the tunnel based on air movement from the ventilation system.

Based on the fact that the majority of these pipes are installed where the temperature of the tunnel would have more of an effect on the temperature – pressure evaluation than the area inside the tank, Willbros asked Pipeline Petroleum Services to re-run their calculations and re-evaluate their inconclusive opinion on the 18-inch and 32-inch lines for Tank-5 by removing the temperature recorded from the tank, in their temperature – pressure evaluation. Pipeline Petroleum Services did that and stated that their conclusions are the same as before. The 18-inch and 32-inch lines passed the volume correction calculations as set forth by the California State Fire Marshal's office but were inconclusive based on the temperature – pressure evaluation.

Willbros spoke to the management of Pipeline Petroleum Services about their conclusions and Pipeline Petroleum Services told Willbros that because of the scrutiny and liability that they would accept with passing these tests, they would not pass if there were any interpretations to be made.

Pipeline Petroleum Services recommendation was to perform a pneumatic test on the lines, to determine if their inconclusive evaluation was correct or not. Willbros was informed by the Navy that a pneumatic test would not be allowed.

Willbros then began analyzing the data supplied by Pipeline Petroleum Services, to determine if the tests were indeed inconclusive or an error was made.

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Willbros performed an analysis of the data and determined the accuracy of the testing equipment to determine if the un-explained  $\Delta P/\Delta T$  is within the accuracy of the testing equipment.

Based on the accuracy of the equipment used during the test and applying these accuracies to the test data, we feel that any test should be deemed acceptable if the unexplained pressure loss or gain that falls within  $\frac{1}{4}$  degree.

Test ID Number: 14-332-02 had an unexplained pressure loss of  $(-3.2 + 1.73) - 1.47$  psig and is within  $\frac{1}{4}$  degree  $\Delta T$  accuracy of 3.57 psig.

Test ID Number 14-332-01A had an unexplained pressure loss of  $(-3.2 + 1.63) - 1.57$  psig and is within  $\frac{1}{4}$  degree  $\Delta T$  accuracy of 5.104 psig.

Test ID Number 14-332-01B had an unexplained pressure loss of  $- 0.10$  psig and is within  $\frac{1}{4}$  degree  $\Delta T$  accuracy of 5.104 psig.

Based on the fact that Pipeline Petroleum Services found that all tests passed the volume correction calculations established by the California State Fire Marshal's office and Willbros determined that all three test performed by Pipeline Petroleum Services falls within  $\frac{1}{4}$  degree of the accuracy of the equipment, Willbros deems that the three tests passed and no test should be considered inconclusive.

It is Willbros recommendation that no further testing of these lines need to be conducted, until the next API 653 examination of Tank-5 is due.



*Justin T. Johnson* 08/20/2014

Justin T. Johnson  
Licensed Professional Engineer No. 23670  
Willbros Engineers (U.S.), LLC  
Oklahoma C.A. No. 144



*Prepared for*

**NAVAL FACILITIES ENGINEERING COMMAND  
ENGINEERING SERVICE CENTER  
Port Hueneme, California**

*Technical Submittal for Project:*

**Project Title: CLEAN, INSPECT, AND REPAIR STORAGE TANKS 5 & 17  
Location: PEARL NAVAL BASE – REDHILL COMPLEX, Pearl Harbor, HI  
Task Order No.: N62583-09-D-0132/0003  
WGS Project Number: 54118  
Date: August 19, 2014**

**TANK 5 HYDROSTATIC TEST RESULTS FOR  
18-INCH AND 32-INCH LINES**

**Submitted By:**  
Willbros Government Services, LLC  
2087 E. 71<sup>st</sup> Street  
Tulsa, OK 74136

Rev	Date	Description	Reviewed	Approved
A	8/19/2014	For Approval	TDA	RGG



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## 1. WILLBROS CONCLUSIONS AND RECOMMENDATIONS

The preliminary report completed by Pipeline Petroleum Services, Inc. and issued to the Navy concluded that the both the 18-inch and 32-inch lines for Tank-5 at Red Hill passed the contract required volume correction calculations as set forth by the California State Fire Marshal's office. Pipeline Petroleum Services stated that the entire test was considered inconclusive in their opinion because each test failed the temperature – pressure evaluation and their thoughts were that there is trapped air into the system and that is why the system failed the temperature – pressure evaluation.

During Willbros review of the report prepared by Pipeline Petroleum Services, it was noted that during testing, the temperature probe in the tunnel recorded a 0.1 °F drop in temperature and the temperature probe in the tank recorded a 2.0 °F rise in temperature.

James Hagen the Project Manager for the Red Hill Tank-5 work informed us that there can easily be a 2.0 °F temperature change in the tank from the tunnel based on air movement from the ventilation system.

Based on the fact that the majority of these pipes are installed where the temperature of the tunnel would have more of an effect on the temperature – pressure evaluation than the area inside the tank, Willbros asked Pipeline Petroleum Services to re-run their calculations and re-evaluate their inconclusive opinion on the 18-inch and 32-inch lines for Tank-5 by removing the temperature recorded from the tank, in their temperature – pressure evaluation. Pipeline Petroleum Services did that and stated that their conclusions are the same as before. The 18-inch and 32-inch lines passed the volume correction calculations as set forth by the California State Fire Marshal's office but were inconclusive based on the temperature – pressure evaluation.

Willbros spoke to the management of Pipeline Petroleum Services about their conclusions and Pipeline Petroleum Services told Willbros that because of the scrutiny and liability that they would accept with passing these tests, they would not pass if there were any interpretations to be made.

Pipeline Petroleum Services recommendation was to perform a pneumatic test on the lines, to determine if their inconclusive evaluation was correct or not. Willbros was informed by the Navy that a pneumatic test would not be allowed.

Willbros then began analyzing the data supplied by Pipeline Petroleum Services, to determine if the tests were indeed inconclusive or an error was made.

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Willbros performed an analysis of the data and determined the accuracy of the testing equipment to determine if the un-explained  $\Delta P/\Delta T$  is within the accuracy of the testing equipment.

Based on the accuracy of the equipment used during the test and applying these accuracies to the test data, we feel that any test should be deemed acceptable if the unexplained pressure loss or gain that falls within  $\frac{1}{4}$  degree.

Test ID Number: 14-332-02 had an unexplained pressure loss of  $(-3.2 + 1.73) - 1.47$  psig and is within  $\frac{1}{4}$  degree  $\Delta T$  accuracy of 3.57 psig.

Test ID Number 14-332-01A had an unexplained pressure loss of  $(-3.2 + 1.63) - 1.57$  psig and is within  $\frac{1}{4}$  degree  $\Delta T$  accuracy of 5.104 psig.

Test ID Number 14-332-01B had an unexplained pressure loss of  $- 0.10$  psig and is within  $\frac{1}{4}$  degree  $\Delta T$  accuracy of 5.104 psig.

Based on the fact that Pipeline Petroleum Services found that all tests passed the volume correction calculations established by the California State Fire Marshal's office and Willbros determined that all three test performed by Pipeline Petroleum Services falls within  $\frac{1}{4}$  degree of the accuracy of the equipment, Willbros deems that the three tests passed and no test should be considered inconclusive.

It is Willbros recommendation that no further testing of these lines need to be conducted, until the next API 653 examination of Tank-5 is due.

**14-332: PRESSURE TESTING REPORT  
OF TANK 5 FUEL LINES**

**Red Hill Underground Fuel Storage Facility  
OAHU, HI**

*Prepared for:*

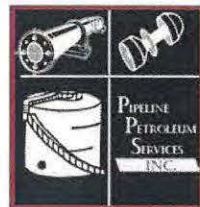


**Willbros Government Services (USA), LLC  
Tulsa, OK**

*Prepared under:*

**Willbros Contract Number: N62583-08-D-0132/003**

*Prepared by:*



**PIPELINE PETROLEUM SERVICES, INC.**  
*1324 Cavalier Blvd  
Chesapeake, Virginia 23323*

**June 23-27, 2014**

## TABLE OF CONTENTS

	<u>Page No.</u>
1.0 EXECUTIVE SUMMARY .....	1
2.0 INTRODUCTION .....	1
3.0 SITE DESCRIPTION .....	1
4.0 TESTING PROTOCOL .....	5
4.1 Test Procedure .....	5
4.2 Test Criteria .....	5
4.3 Tester Qualifications .....	7
4.4 Test Section Descriptions .....	7
5.0 TESTING RESULTS.....	7
5.1 Testing Activities.....	8
6.0 CONCLUSIONS AND RECOMMENDATIONS .....	10
6.1 Conclusions .....	10
6.2 Recommendations .....	14
7.0 REFERENCES .....	16

## LIST OF APPENDICES

Appendix A	Project Photographs
Appendix B	Field Notes & Daily Activities
Appendix C	Test ID 14-332-01A & B / Test ID 14-332-02 Detailed Test Results
Appendix D	Raw Test Data from Dataloggers (18"Ø & 32"Ø lines)
Appendix E	Instrument Calibration Certificates

## LIST OF ABBREVIATIONS AND ACRONYMS

• MAOP: Maximum Allowable Operating Pressure	• MAWP: Maximum Allowable Working Pressure
• PRV: Pressure Relief Valve	• MOV: Motor Operated Valve
• DBB: Double Block & Bleed Valve	• HPV: High Point Vent
• LPD: Low Point Drain	• SS: Stainless Steel
• CS: Carbon Steel	• AG: Aboveground
• UG: Underground	• NPT: National Pipe Thread
• PSI: Pounds / Square Inch	• WOG: Water or Gas
• CP: Cathodic Protection	• AST: Aboveground Storage Tank
• UST: Underground Storage Tank	• PIT: Pressure Indicating Transmitter

## 1.0 EXECUTIVE SUMMARY

The scope of this project is to perform point-in-time hydrostatic pressure testing of the Tank 5 fuel lines at the Red Hill Underground Fuel Farm, Oahu, HI. The testing was performed and documented in accordance with the Willbros Pressure Test Procedure NDT-3, Revision 9, Dated June 5, 2014, as well as "Pressure Testing Requirements for Hazardous Liquid Pipelines in California", Office of the State Fire Marshal, Pipeline Safety Division, May 2011 Revision (CSFM) and "Operation & Maintenance: Maintenance of Petroleum Systems" United Facilities Criteria (UFC) UFC 3-460-03F, January 2003, which is the jurisdictional Government regulation of Military Petroleum Facilities. The tested lines were tested to cross-country and process hazardous liquid pipeline testing standards since an API-653 hydrostatic test was not feasible at this time.

The Tank 5 lines are actually classified as tank nozzles from the skin valve flange to the wall of the tank and consisted of one 32"Ø F-76 line and one 18"Ø JP-8 line, each between 50-70 feet in length located directly beneath the tank. The lines were hydrostatically pressure tested between the dates of June 23, 2014 and June 27, 2014 at 1.5 times (150%) the maximum allowable operating pressure of 108 psi for four hours. The test pressure was calculated by factoring the maximum head of a full tank calculated by  $(.433)(SG)(Height)$ :  $(.433 \text{ (psi / ft head - fresh water)})(1.0 \text{ (Specific gravity of fresh water)})(250' \text{ (Height of Tank 5)}) = 108.25 \text{ psi} \times 150\% = 162.375 \text{ psi}$ .

The CSFM pass / fail criteria was chosen by the Navy to determine the success of each test base on volume gain / loss calculations based on temperature change. Strictly based on the volume loss criteria established by the CSFM both tests passed, however neither line fully stabilized and the temperature / pressure evaluation of expected pressure change vs the actual pressure change, while very close, did not achieve a passing result. Because of the conflicting calculation results, both test attempts are inconclusive pending the result of the recommended pneumatic test.

The recommendation from PPSI at this time is to perform pneumatic testing of both lines to positively confirm or deny the existence of trapped vapor preventing a successful hydrotest.

## 2.0 INTRODUCTION

Willbros Government Services (WGS) contracted Pipeline Petroleum Services, Inc. (PPSI) to perform temperature compensated hydrostatic pressure testing of the Tank 5 issue / receipt lines located at the Red Hill Underground Fuel Facility, Oahu, HI.

The testing under this cover was performed to determine integrity of these lines in the absence of an API-653 hydrotest.

## 3.0 SITE DESCRIPTION

The Red Hill Underground Fuel Facility is located on the island of Oahu, HI approximately 3 miles due east of Pearl Harbor. The Red Hill fuel farm is a classified facility and consists of 20 underground tanks approximately 250' tall x 100' in diameter with an estimated capacity of 12.5 million gallons each, as well as underground pumping facilities, line networks, and multiple access points. The facility receives jet propulsion fuel (JP-8 & JP-5), as well as marine diesel fuel (DFM / F-76) from tankers as well as from a trans-island line and dispenses to trucks at the truck rack and to navy ships from

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Red Hill Fuel Farm, Oahu, HI

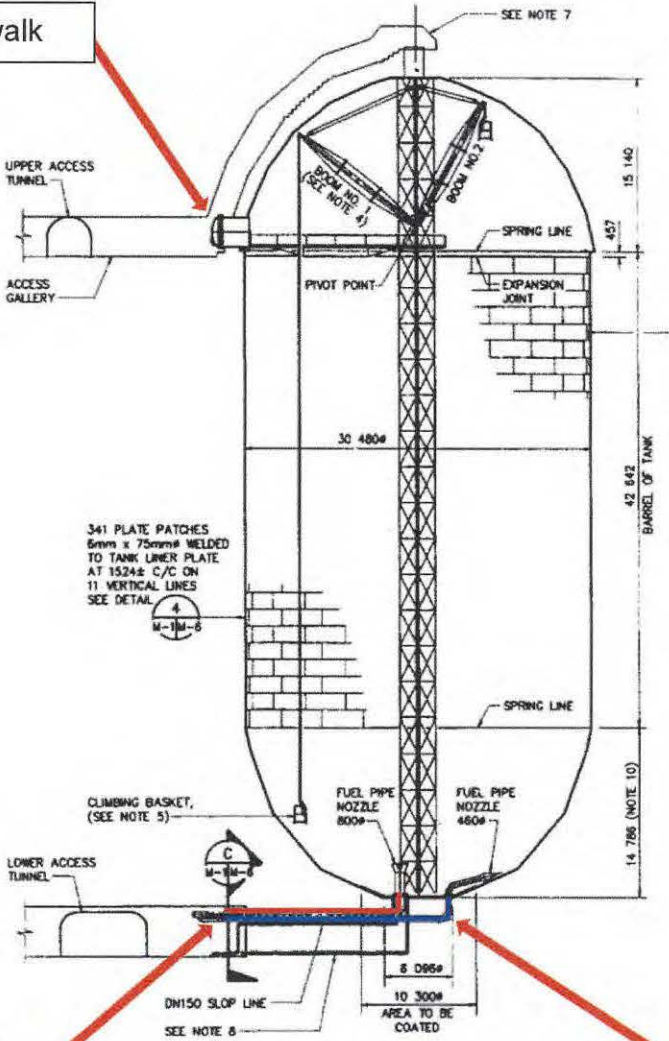
several piers. The facility issues to Pearl Harbor by gravity and pumps located in PH 59 are used to recirculate or pump back up to Red Hill.

Testing was performed on the Tank 5 dual purpose issue / receipt lines for F-76 & JP-8. Refer to Figure 3-1 on the following page: Tank 5 Layout.



Figure 3-1: Tank 5 Layout (Identical to all Red Hill Tanks)

Tank Manway & Access Catwalk



Test Sections:  
 Red: 32"Ø F-76 Piping  
 Blue: 18"Ø JP-8 Piping

Tank skin valves removed at this location and test blinds installed.

Test Section Lines

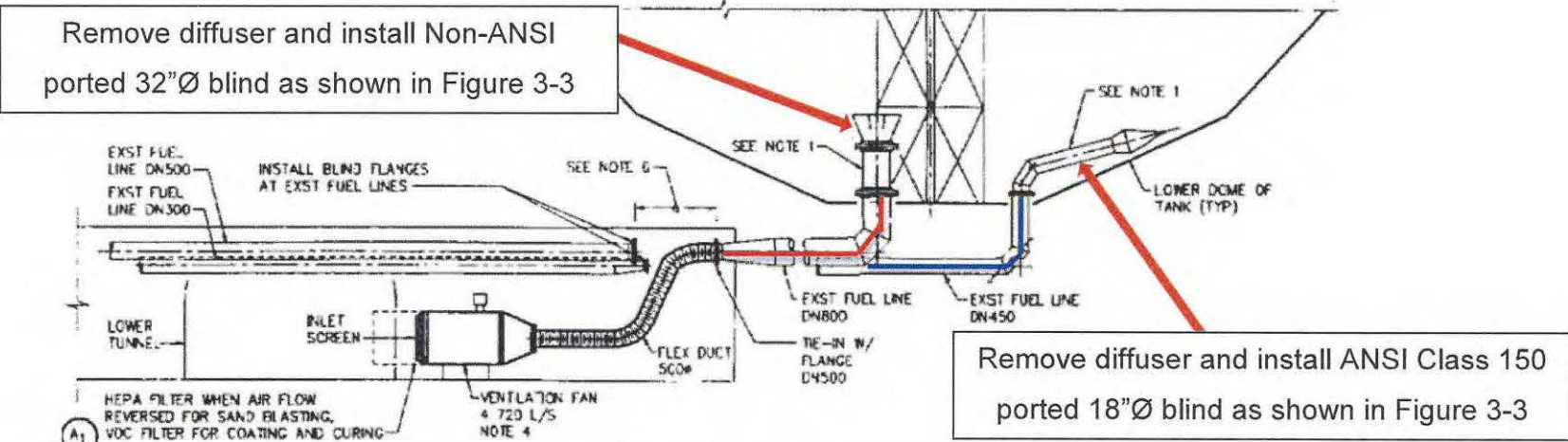


Figure 3-2: Test Sections at bottom of tank. Blue: 18"Ø JP-8 line / Red: 32"Ø F-76 line.

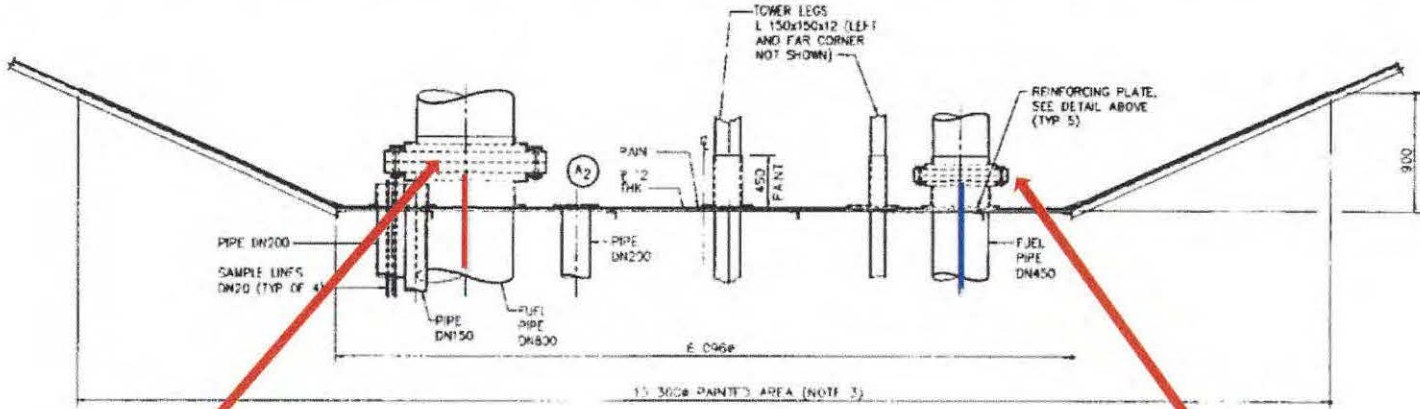


Figure 3-3: Test Sections: Inside of tank detail.

Remove diffuser and install Non-ANSI ported 32"Ø blind here

Remove diffuser and install ANSI Class 150 ported 18"Ø blind here

## 4.0 TESTING PROTOCOL

### 4.1 Test Procedure

Testing procedures used were performed in conformance (In part) with United Facilities Criteria (UFC) UFC 3-460-03F (Reference 7.1), California State Fire Marshal's (CSFM's) Pressure Testing Requirements for Hazardous Liquid Pipelines (Reference 7.2), American Society of Mechanical Engineers (ASME) B31.3: Process Piping (Reference 7.3) & ASME B31.4: Pipeline Transportation Systems for Liquid Hydrocarbons and Other Liquids (Reference 7.4) and with Section 3.4 of American Petroleum Institute's Recommend Practice 1110 (API RP-1110): Pressure Testing of Liquid Petroleum Pipelines (Reference 7.5).

These testing procedures are not normally applied to tanks, but cross country and process pipelines. Since a normal API-653 hydrostatic test was not feasible, these procedures were chosen.

The procedure on site also satisfies the Willbros Pressure Test Procedure NDT-3, Revision 9, Dated June 5, 2014. (Reference 7.6)

### 4.2 Test Criteria

The acceptance criteria for this project is based on criteria established (In part) in API RP-1110, CSFM, test volume and temperature compensation calculations, no visual evidence of leaks, and accepted industry practice.

This testing satisfies the requirements of UFC 3 460 03F for a five-year hydrostatic test.

The requirements for UFC are listed below:

*2.3.3. Pipeline Testing. Pipelines must be tested annually for leaks. The MAJCOM fuels engineer may authorize an equivalent methodology as long as state environmental requirements are met. Pressure tests are affected by weather, so it is best to do them in the spring or fall when fuel, ground, and air temperatures are similar. An overcast day or early in the morning would be preferable to lessen the solar effects on aboveground lines. Maintain all leak test records in the LFM shop for five years unless environmental requirements dictate longer. Send copies of these records to the MAJCOM fuels engineer if requested. Use the following testing approach unless state requirements are more stringent:*

*2.3.3.1. Annual Pressure Testing. Pressure-test all on-base fuel piping systems annually using existing system pumps. Pressurize unloading, loading, transfer, and hydrant dispensing piping systems by running the appropriate pumps against a closed system until deadhead pressure is reached. Close appropriate valves to trap this pressure in the system, then turn off the pumps. NOTE: Some ball valves do not provide isolation and require a differential pressure (DP) to seat, so blind flanges may be required. Take pressure gauge readings within fifteen minutes after allowing sufficient time for the fuel pressure to stabilize. Visually check all aboveground piping and piping in concrete pits for leaks. Audibly check closed valves for sound as evidence of an internal valve leak. If no visible or audible leaks occur, then take pressure gauge readings every fifteen minutes for the first hour, and once every half-hour for the next hour. Total time for the pressure test will be two hours. Document all pressure tests by recording the following:*

*2.3.3.1.1. Name of system test (i.e., refuel header, defuel header, lateral pipelines). Provide facility number.*

*2.3.3.1.2. Date of test and weather conditions (e.g., sunny and 27 °C [80 °F]; cloudy and 18° C [64 °F]). NOTE: Record any weather change during the test period.*

*2.3.3.1.3. Pressure readings:*

*2.3.3.1.3.1. Start (approximate local time) pressure.*

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Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI

2.3.3.1.3.2. Fifteen minutes (approximate local time) pressure.

2.3.3.1.3.3. Thirty minutes (approximate local time) pressure.

2.3.3.1.3.4. Forty-five minutes (approximate local time) pressure.

2.3.3.1.3.5. One hour (approximate local time) pressure.

2.3.3.1.3.6. One and one-half hours (approximate local time) pressure.

2.3.3.1.3.7. Two hours (approximate local time) pressure.

2.3.3.2. *Five-Year Hydrostatic Test.* Perform a hydrostatic pressure test every five years on all underground fuel transfer pipelines (product is typically the test media for this test). The MAJCOM fuels engineer sets the specific year. A hand-operated hydraulic pump, or equivalent with a built-in reservoir tank supplies hydrostatic pressure. This takes the place of the annual pressure test. The hydrostatic test may be conducted using a dual-pressure, temperature-compensating pressure test conducted at the same pressure specified in paragraph 2.3.3.2.2 with MAJCOM fuels engineer approval. The test vendor must have an independent third-party review of the test.

2.3.3.2.1. To test the pipe, first isolate the section being tested with blind or spectacle flanges. If DBB valves will hold the pressure, blind flanging is not required. **NOTE:** filter/separators (F/Ss), thermal relief valves, safety valves, and sight glasses may have to be removed or isolated by blind/skillets.

2.3.3.2.2. Using a hand-operated hydrostatic pump, perform a static pressure test to the lesser of 1.5 times the system dead head pressure or 1.896 megapascals (275 pounds per square inch gauge) maximum. Use fuel to perform all tests. Pressure may also be applied with a dead-weight tester or suitable motor-driven pump.

2.3.3.2.3. Once the pressure is stabilized, record the pressure every 15 minutes for the first hour, every 30 minutes the second hour, then every hour thereafter. If at the end of the minimum four-hour test (the longest test possible is recommended preferably overnight) no leaks are found, further testing is not required. (Use the procedure described in paragraph 2.3.3.1.) If a leak or excessive pressure change is observed, perform a flow test by repressurizing the line with the hydrostatic pump. Measure and record the amount of fluid required to maintain this pressure for four hours. If a leak is found, contact the environmental flight and take action to repair it. Also, promptly notify the command fuels engineer and DESC if additional funding is required for repairs, leak detection, and or location. A drop in pressure could be the result of a decrease in product temperature or absorption by the product of air in the line. To rule this out, you may repressurize the line and extend the test period to at least 24 hours.

The requirement and the intent of the Regulation(s) is not just to strength test the pipeline or system; it is to confirm the tightness of the system to the extent possible, which is the reason we feel the test results under this cover are inconclusive at this time. (See test results)

The procedure and criteria used under this report cover is to calculate the tightness of the system by reconciling any pressure loss / gain with pipeline temperature, compressibility of the test media, pipeline material coefficient of expansion, and by converting fluid gain / loss into equivalent pressure change to ensure that the test results actually confirm or deny that the pipeline is suspected of leaking.

The calculations used are based on the CSFM Appendix C Standard Pressure / Temperature Formulas as shown below:



Appendix C – Standard Formulas used for Pressure / Temperature Calculations

CSFM Standardized formula for performing pressure – temperature calculations to determine volume change.

Basic Formula:  $\Delta V / V = Kp \Delta P + Kt \Delta T$

Where:  $Kp = [(D / t)(5 / 4 - \mu) / E] + 1 / \beta = (1.9 D / 2 E t) + 1 / \beta$

And:  $Kt = 3a - g$

- $\Delta P$  = Liquid Pressure Change
- $\Delta T$  = Liquid Temperature Change
- $\Delta V$  = Liquid Volume added to that inside the pipe (negative if flows out)
- $V$  = Nominal Pipe Volume =  $\pi D^2 L / 4$
- $D$  = Inside Pipe Diameter
- $L$  = Pipe Length
- $t$  = Pipe wall thickness
- $\mu$  = Poisson's ratio = 0.3
- $E$  = Young's Modulus =  $30 * 10^6$  psi
- $\beta$  = Liquid Bulk Modulus, a function of Pressure and Temperature
- $g$  = Liquid Volumetric expansion coefficient, a function of Pressure and Temperature
- $a$  = Linear coefficient of Thermal Expansion =  $6.5 * 10^{-6} 1/^\circ F$

**4.3 Tester Qualifications**

The supervisor on site (Dennis Cobb) during testing has over twenty (20) years of pressure testing experience with a working knowledge of applicable regulations and test standards.

**4.4 Test Section Descriptions**

Testing on the Tank 5 fuel issue / receipt lines was conducted on the dates indicated. Table 4-1: Test Sections and Appendix C provide details of each test section and configuration.

Table 4-1: Test Sections

Test Section Identification	Designation	Diameter (Inches)	Length (Feet)	Volume (Gallons)	Comments
14-332-01A & B	32"Ø F-76	32" / 20"	48	1838	Length was calculated by using the total volume pumped into the line sections as well as using the head pressure to determine the vertical rise, therefore the length is estimated.
14-332-02	18"Ø JP-8	18" / 12"	65 (Estimate 61' of 18"Ø & 4' of 12"Ø)	764	Length calculated same as the 32" line.

Note: Test sections could not be physically measured during testing because they are encased in concrete.

**5.0 TESTING RESULTS**

Detailed test results for the 18"Ø & 32"Ø test sections are provided in Appendix C. The 32"Ø test results are from the 4 hour test period on 6/26/14 from 20:00 to 24:00 and the theoretical test using the last 45 minutes of data from the following morning. The 18"Ø test results are from a test period derived from the datalogger data that was recorded overnight from 10:37 PM on 6/25/14 to 01:37 AM on 6/26/14. The result for both tests from the CSFM volume correction calculations is a passed test, however the result from



the temperature evaluation is a failed test. We feel that based on the conflicting results of the test calculations, the margin of error with the unknown variables such as actual volume of the reducers in the line and the actual pipe specification and grade, and the inherent margin of error with hydrotesting, that the result is inconclusive at this time. The rate of decay and non-stabilization could be the result of trapped air or a leak and it is impossible to determine which at this time.

Test results are listed in Table 5-1.

Table 5-1: Test Results

Test Section Identification	Designation	Length (Feet)	Volume (Gallons)	Test Date	Result
14-332-01A	32"Ø F-76	48	1838	6/26/14	Passed CSFM Volume Correction Calculations / Failed temperature – pressure evaluation. Inconclusive – Recommend Pneumatic testing to confirm presence of trapped vapor.
14-332-01B	32"Ø F-76	48	1838	6/27/14	Passed CSFM Volume Correction Calculations. Temperature – pressure evaluation results much closer than in Test A due to apparent stabilization overnight, however the final result remains inconclusive.
14-332-02	18"Ø JP-8	65	764	6/25/14 & 6/26/14	Passed CSFM Volume Correction Calculations / Failed temperature – pressure evaluation. Inconclusive – Recommend Pneumatic testing to confirm presence of trapped vapor.

### 5.1 Testing Activities

We attempted to pressurize, stabilize, and test both test sections several times and exhausted all known methods to obtain a successful hydrotest. We ensured that there were no leaks on any external feature that we could control and even modified our test equipment to ensure no air was trapped at that point that would affect the tests. Excessive amounts of time were expended trying to re-pressurize and stabilize to try and compress any trapped air in both test sections.

The following is the official test charts from the dataloggers for both test periods. The charts clearly show all pressurizations, depressurizations, logger movements to replace the flange gaskets, and the relative stability of the temperature in the tunnel while the temperature inside the tank fluctuated between 2-4°F indicating it was affected by the ambient air differences in the tank. Also seen clearly is the relative stability of all lines towards the end of the logging period for the 32"Ø test.

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Red Hill Fuel Farm, Oahu, HI

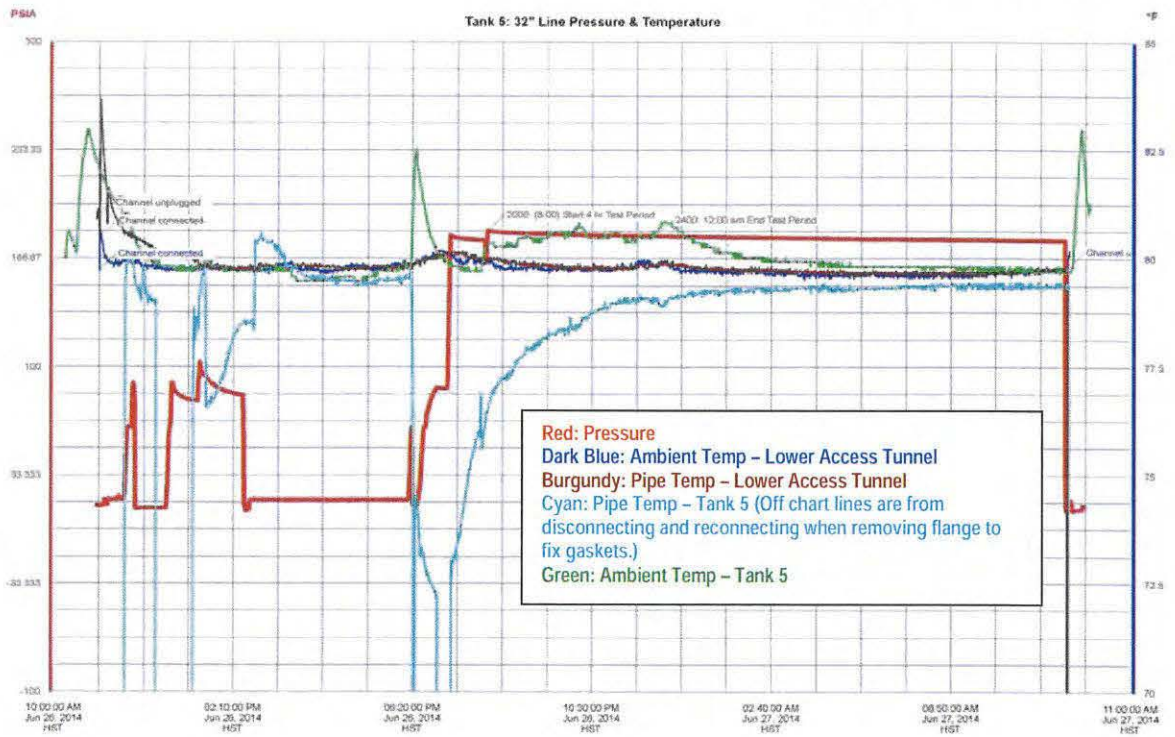


Figure 5-1: Test data chart from the 32"Ø testing attempts.

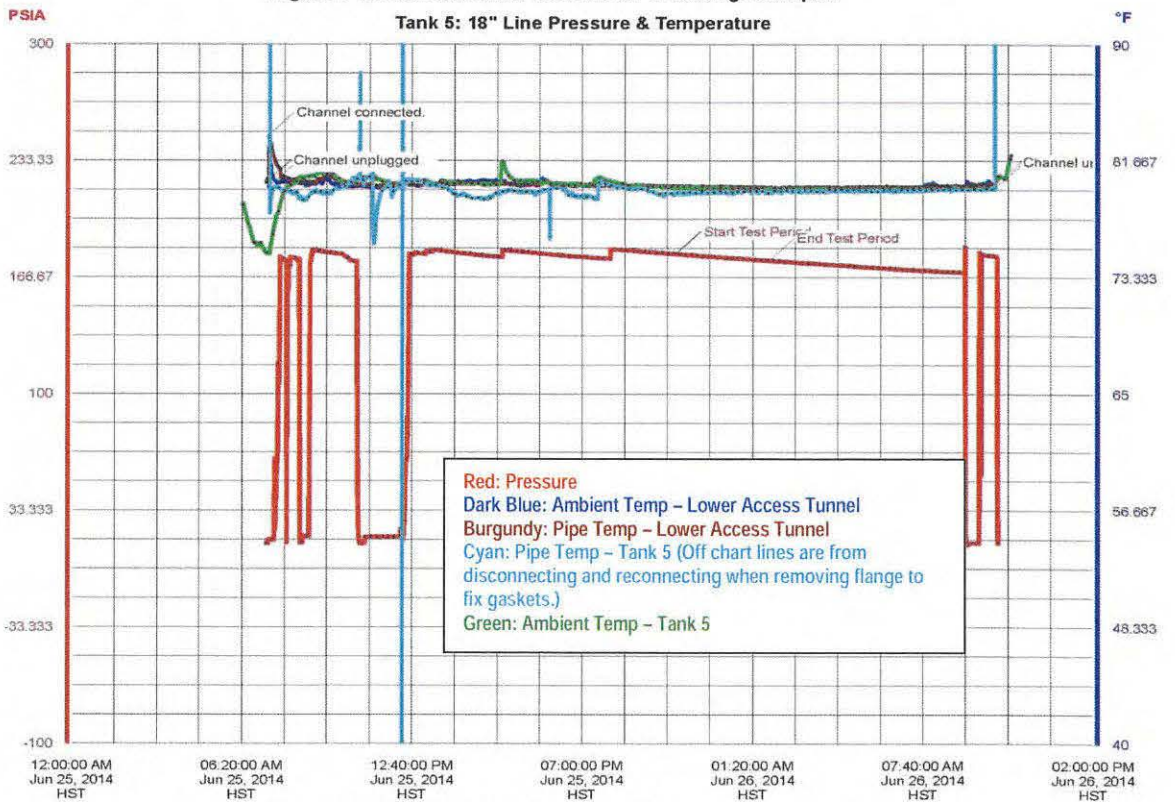


Figure 5-2: Test data chart from the 18"Ø testing attempts.



## 6.0 CONCLUSIONS AND RECOMMENDATIONS

### 6.1 Conclusions

This hydrostatic pressure testing of the subject lines are not considered precision volumetric leak detection testing. The testing performed is classified as a point-in-time, pressure decay combination strength / stress / leak test of the line system against the test blinds to determine if there is a suspected leak to the extent possible.

Testing was performed per the jurisdictional regulatory requirements of United Facilities Criteria (UFC) UFC 3-460-03F (United Facilities Criteria) and the test procedures used were performed in conformance with (In part) API-RP-1110, CSFM (California State Fire Marshall – State Lands Commission Hydrotesting Procedures), and the Willbros Pressure Test Procedure: NDT-3.

**The lines passed the CSFM volume correction calculations, however experienced pressure loss that could be attributed to trapped air in the test sections, which caused the pressure / temperature evaluation to fail. Because of this both tests are considered inconclusive at this time.**

This determination is based on criteria established (In part) in API-RP-1110, CSFM, as well as, test volume and temperature compensation calculations, no visual evidence of leaks on exposed portions of the lines in the tunnel and inside of the tank, and accepted industry practice.

We were unable to stabilize either line due to suspected trapped vapor in the lines. We are forced to conclude at this time that trapped vapor is the cause of the pressure loss observed because of the extremely small rate of pressure loss and the rate of pressure loss decreased as time passed. It should be noted that a leak, if present, would also experience a decrease in the leak rate as the pressure decreased in the same manner as dissolution of trapped air into the test medium.

While this loss of pressure could be attributed to a small leak, a pneumatic test must be performed to rule exclude the possibility of trapped air before the line(s) can be considered a failure.

If the pneumatic test is successful then an engineering evaluation can be performed to accept the lines as a successful test using tracer testing or another method of leak detection that is not affected by trapped vapor.

If the pneumatic testing is not successful, the line(s) would then be considered a failure and must be repaired or taken out of service.

In addition, if the pneumatic testing proves successful and the determination is that the line(s) are tight, that determination does not guarantee that the line(s) will

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**Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI**

not leak in the future. This is important because there has been some visual evidence of pitting on the interior surface of the 32"Ø line prior to our arrival.

See the Section 6.2 titled "Recommendations" for a sample procedure used by PPSI on other projects to confirm or deny the existence of trapped air.

Figures 6-1 and 6-2 on the following two pages illustrate possible locations of trapped air in each test section for consideration. They are not meant to depict the actual configuration of the pipe sections.

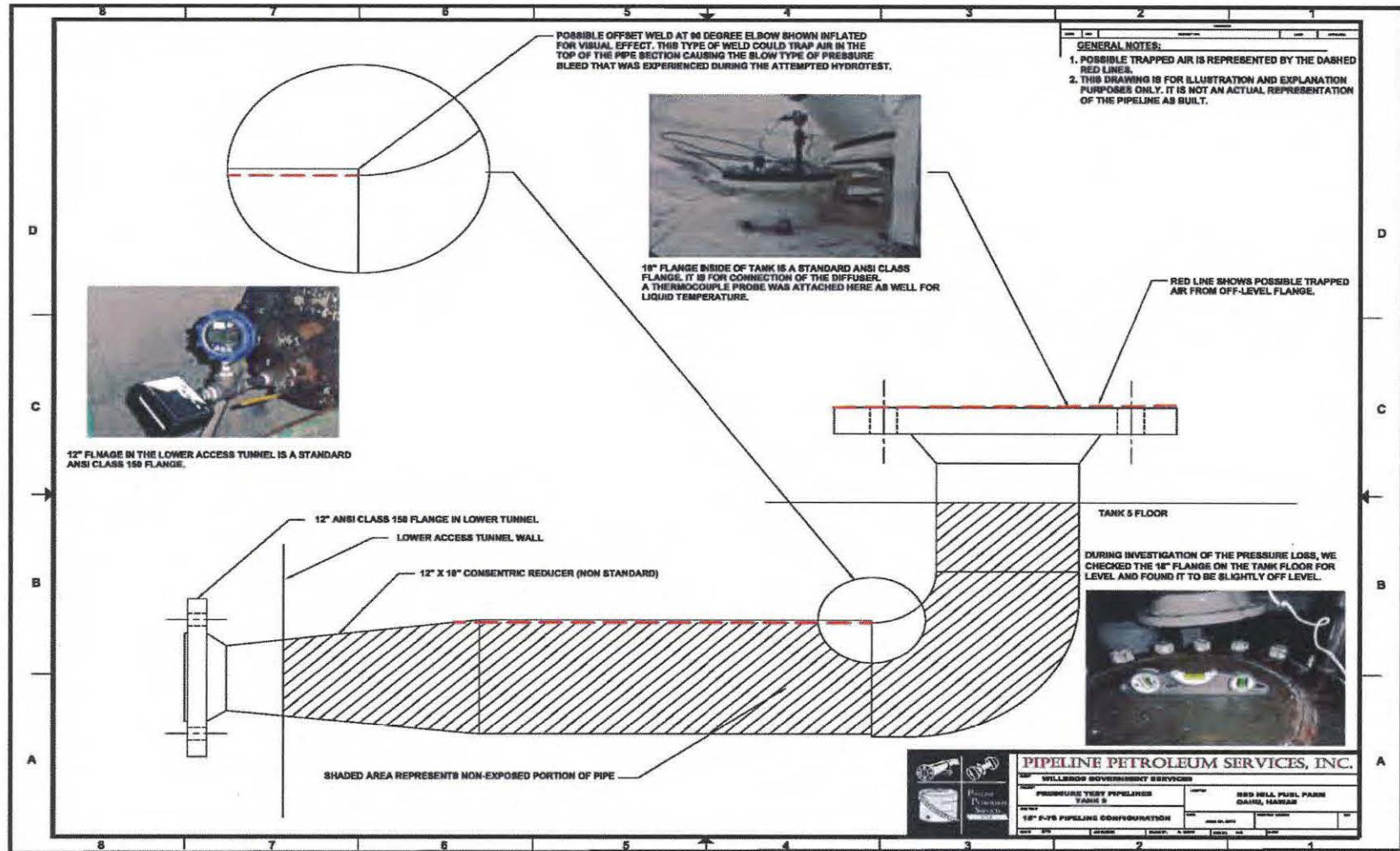


Figure 6-1: Drawing of the 18"Ø line explaining possible trapped air scenarios.



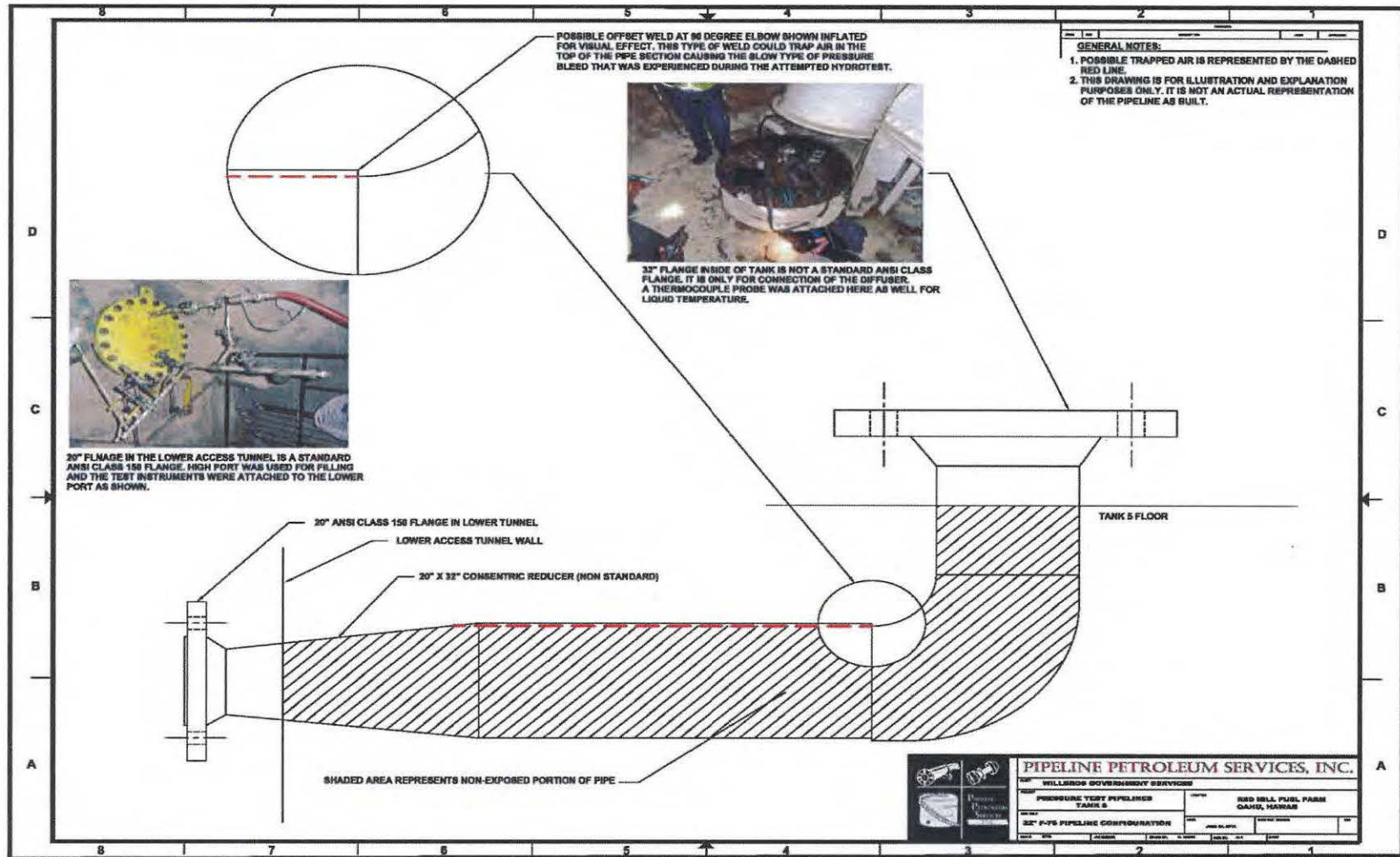


Figure 6-2: Drawing of the 32"Ø line explaining possible trapped air scenarios.

## 6.2 Recommendations

Due to our inability to stabilize the test sections at the Red Hill, Tank 5 site with trapped air hindering our hydro testing attempts, we recommend to use preliminary pneumatic tests to verify in the field if the lines were leaking or if the pressure loss was due to trapped air.

During the pressurization attempts and hydrostatic testing attempts, we followed an order of operations developed by PPSI using past experience to follow in case of pressure loss to determine in a logical order if the cause is a leaking valve, trapped air, or an actual leak in the line. We knew in this instance there was only two causes for the pressure loss; trapped air in the line or a leak. On each line test section we used the following order of operations in troubleshooting the loss of pressure:

1. Initial pressurization and air bleed. Allow reasonable stabilization period and repressurize if necessary.
2. Identify any suspect fittings or flanges / gaskets. Repressurize and stabilize.
3. Identify any other areas that could possibly trap air.
4. Repressurize final time.
5. **Next Recommendation:** Pump line down to extent possible and pressurize with compressed air to 25 psi and hold. If line does not experience a decrease in pressure with the compressed air, the problem is trapped air in the line and steps need to be taken to further modify the line so a successful hydro-test can be accomplished if that is the final desire.

### **Proposed Pneumatic Test Procedure**

The following pneumatic test procedure has been developed and has been used by PPSI successfully several times at other sites.

ASME B 31.3 Section 345.5 addresses pneumatic testing as does ASME B 31.4 Section 437.4.3. Only the B 31.4 standard specifies a duration of one hour for a leak check.

#### **I. Hydrostatic Testing Discontinue Criteria**

1. Line is 100% isolated either by DBB valves (Check cavities for leaks), installation of skillets, or removal of valves and blinding. **Completed – testing up against ported test blinds.**
2. Air has been bled to extent possible and system investigated for other possible causes of pressure loss. **Completed – see notes in this report.**
3. Line has been pressurized up to 5 times in an attempt to stabilize and left overnight at least one night for stabilization. **Completed with no real success.**

## II. Pneumatic Test Criteria

ASME B31.4 only allows for pneumatic testing for piping operated at a hoop stress less than 20% of the SMYS of the pipe. Since we don't know what the SMYS of this piping is, we will limit any pneumatic test pressures to 25 psi (IAW ASME B31.3). The purpose of this test is not to specifically satisfy ASME B31.4; it is to confirm the line is subjected to trapped air preventing a successful hydrotest and to confirm that the line is not actually leaking causing the loss of pressure in the initial hydrostatic test.

1. Pump as much liquid as possible from line after removal of the test blinds.
2. Test line at determined pressure for 4 hours. Soap all joints, flanges, and threaded fittings during test period. Test pressure as described in ASME documents is 110% of the design pressure or MAOP. Again, we feel a 25 psi test is more than sufficient to confirm trapped air in the hydrotest.

**Under the circumstances that we are proposing a pneumatic test and the intent that the pneumatic testing will be utilized, we feel that a 25 psi test would suffice for determining if the lines are leaking or not. Pneumatic testing is inherently dangerous and that risk factor is multiplied as the pressure increases.**

3. Testing gas shall be compressed air as there is no petroleum in the line and the tank is currently out of service.
4. Pass / Fail criteria shall be no loss of pressure for duration. All visual inspection requirements remain the same.
5. All parties must concur with the test result.
6. ASME PCC-2 should be used to calculate a safe distance from the piping during testing. This area will be physically isolated for the test duration.

Should any questions about this report or the information contained herein arise, contact Mr. Dennis Cobb, Vice President / Owner at (757) 544-0831 or by email at [dcobb@pipelinepsi.com](mailto:dcobb@pipelinepsi.com).

## 7.0 REFERENCES

- 7.1 "Operation & Maintenance: Maintenance of Petroleum Systems" United Facilities Criteria (UFC) UFC 3-460-03F, January 2003
- 7.2 "Pressure Testing Requirements for Hazardous Liquid Pipelines in California", Office of the State Fire Marshal, Pipeline Safety Division, May 2011 Revision
- 7.3 American Society of Mechanical Engineers, "Standard B31.3: Process Piping", 2009
- 7.4 American Society of Mechanical Engineers, "Standard B31.4: Pipeline Transportation Systems for Liquid Hydrocarbons and Other Liquids", 2009
- 7.5 American Petroleum Institute, "Recommended Practice 1110: Pressure Testing of Steel Pipelines for the Transportation of Gas, Petroleum Gas, Hazardous Liquids, or Carbon Dioxide", Sixth Edition, February 2013
- 7.6 Willbros Government Services, "Pressure Test Procedure: NDT-3", Revision 9, June 5, 2014

*APPENDIX A –*

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*PROJECT PHOTOGRAPHS*



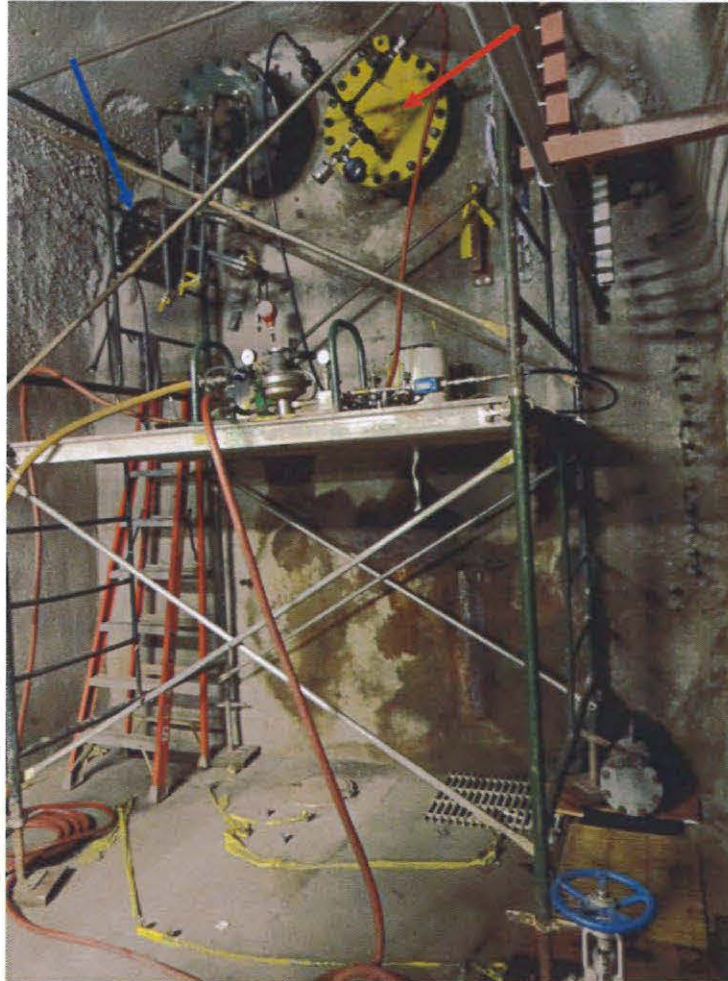


Figure 1.0: Test connections for the 32" F-76 (Red) and 18" JP-8 (Blue) lines located in the lower access tunnel.

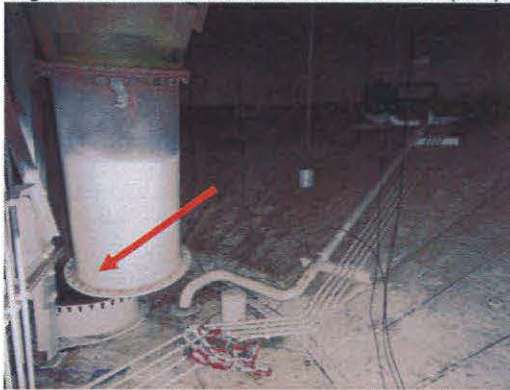


Figure 2.0: The 32" line was prepared for testing by removing the diffuser and installing a ported blind on the pipe flange as indicated. This connection was not a standard ANSI flange and required a custom ported blind to be fabricated. This flange was also not even and required several attempts to seal using different combinations of gaskets of various materials.



Figure 3.0: The 18" line was prepared for testing by removing the diffuser and installing a ported blind on the pipe flange as indicated. This connection was a standard ANSI Class 150 flange.

PIPELINE PETROLEUM SERVICES, INC.

Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI



Figure 4.0: Test tree on the 12"Ø flange in the lower access tunnel for the 18"Ø line.



Figure 5.0: As a precaution against possible air entrapment, we removed our test tree and connected the test instruments directly to the pipe in an effort to stabilize the pipe. The efforts were not successful.



Figure 6.0: The 18"Ø line inside of Tank 5. Note temperature probe connected to the port on the blind flange.



Figure 7.0: As we exhausted methods to rule out trapped air in the 18"Ø line, we decided to see if the level of the flange inside of the tank could trap a small amount of air and the conclusion is yes. (See drawing 6-1)



Figure 8.0: There was a small notch cut from the flange of the 32"Ø line inside of the tank. This notch was the source of some of the leaks that proved difficult to overcome on the 32"Ø flange.

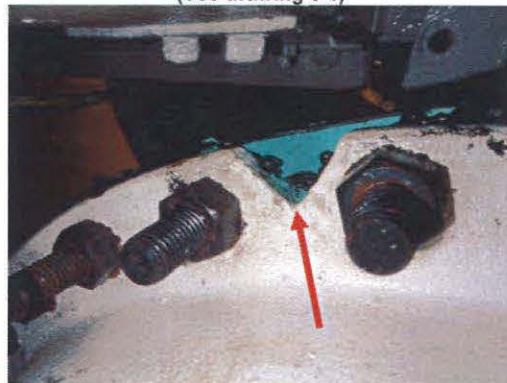


Figure 9.0: Close view of the notch identified in Figure 8.0. A thick ¼" neoprene gasket finally allowed us to seal the flange.





Figure 10.0: The 32"Ø pipe was drained just enough to remove the flange to change the gasket. We confirmed that there was little room for trapped air at this point.



Figure 11.0: The custom fabricated 32"Ø ported flange supplied by WGS is shown here.



Figure 12.0: One of the failed attempts at pressurizing the 32"Ø line. Note active leaks form the bolts due to the gasket not ssealing.



Figure 13.0: 910 ml was drained from the 32" line during the DV / DP check.

*APPENDIX B –*

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*FIELD NOTES & DAILY ACTIVITIES*

PIPELINE PETROLEUM SERVICES, INC.

Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI

**Willbros - Red Hill – Tank 5 Daily Notes Day 1 and 2**

6/23/14 – **0600** – Onsite. We met with James Hagen (Willbros). Take a tour of upper and lower tunnels and Tank 5 to familiarize ourselves with the site. **0800** – Meeting with NAVFAC, Navy, and Willbros personnel to discuss scope of work and safety. **0900** – Site walk through and evaluation with all personnel. **1200** – Connect test equipment to 20" flange (for 32" pipe) inside the lower access tunnel while connecting a temperature probe and bleeder equipment inside tank. **1323** – Start pumping water into line with 1" hose from water main inside of the lower access tunnel. **1546** – Pumped in approximately **1832.99** gals in thus far and 3.3 psi on the line. Personnel from inside the tank indicate that there are leaks coming from the bolts of the flange inside the tank. We stopped pumping water and secured. Crew decided to get a new gasket for the flange and change it tomorrow. **1700** – Left site for the day.

6/24/14 – **0600** – Onsite. Sign in and Safety briefing. **0700** – Willbros personnel make up gasket for 32" flange from garlok material supplied by the facility (Per Scott Hedricks) and install it. There was estimated 3 gallons of water on tank floor due to leaking bolts the day before. Dry up water using buckets and rags. **0839** – Start pumping water into the line. **0842** – We have **1839.03** gals in and 48.7 psi on the line from the normal water main pressure. We bled off 2.12 gals (All Pressure – down to 0 psi) to allow crew inside of tank to put temp probe on line. Cut on water again from the main, added 2 gals and pressure went back up to 48.3 psi. **1022** – Start pressurizing line with pressure pump supplied by Willbros. Again, there were leaks inside tank from several bolts. We stopped operations. D. Cobb and James Hagen go into the tank to identify the leaks. **1111** – Bleed off pressure. It was confirmed that the gasket needed to be replaced with a different combination. **1245** – Crew went to get silicone and Willbros personnel make up 2 more gaskets. **1330** – D. Cobb, James and Willbros personnel entered tank to install new gaskets and apply silicone. Let sit overnight to fully cure. **1500** – Drain approximately 20 gallons from 32" line so flange can be removed. **1530** – Connect fittings and water hose to 12" flange (for 18" pipe). **1542** – Start pumping water into line. **1642** – Add **761.69** gallons to the line. Bleed air from the ported blind inside of tank. We disconnected the water hose and attached our pressure testing equipment / sensors to the pipe. **1700** – All personnel met upper level tunnel at Tank 5 and discuss the next day plan of work. **1745** – Left site for the day.

**Willbros - Red Hill – Tank 5 Daily Notes Day 3**

6/25/14 – **0600** – Onsite. Sign in and Safety briefing. **0700** – Start pressurizing 18" line from 0 psi to 47 psi with head pressure from water hose thru the pump (1.65 gals in). **0742** – Start pressurizing up using pump. **0745** – Pressure at 102.2 psi (total 2.3 gals in). Bleed down 10 psi to 92.2 psi into measuring cup (340mil) for DV / DP check. Resume pressurizing line. **0747** – Pressure at 163.0 psi. (2.66 gals in) Let stabilize. **0800** – Pressure at 161.1 psi. Bleed air to 157.8 psi and re-pressurized. **0810** – Pressure at 162.8 psi (2.67 gals in total). Let Stabilize. We tightened up our pressure recorder (Madgetech Unit 1) after a minor drip was observed. Pressure is still decreasing. **0852** – Pressure at 160.2 psi. Re-pressurize again. **0857** – Pressure at 166.5 psi (2.68 gals in total). Let Stabilize. **0920** – **START TEST....** Take first readings. **0921** – Crew inside of the tank called on radio, we have several more leaks from bolts on the flange inside the tank. Crew attempted to stop the leaks with hammer wrenches. **0935** – **STOP TEST!** D. Cobb and James Hagen went into the tank and identify leaks. They used hammer wrenches again to try to stop the leaks. **1030** – Pressure at 160.2 psi. **1035** – Pressure at 160.0 psi and still dropping. **1040** – Bleed off pressure and change gasket. **1220** – Start pressurizing line by using water thru the pump. **1235** – Pressure at 48.0 psi (3.95 gals in). Start using pump to pressure up line. **1238** – Pressure at 164.7 psi (4.29 gals in total). Let Stabilize. **1243** – Pressure at 164.2 psi. Re-pressurize to 165.3 (4.29 gals in total). Let Stabilize. **1308** – Pressure at 164.8 psi. Re-pressurize to 166.2 psi (4.29 gals in total). Let stabilize. **1325** – Pressure at 164.4 psi. Re-pressurize to 166.9 psi (4.29 gals in total). Let stabilize. **1559** – Pressure at 162.7 psi. **1600** – Re-pressurize to 166.9 psi (5.31 gals in total). Let stabilize. **1720** – Pressure at 164.9 psi. **1740** – Pressure at 164.5 psi. **1800** – Pressure at 163.9 psi. **1820** – Pressure at 163.6 psi. **1845** – Pressure at 163.1 psi. **1900** – Pressure at 162.7 psi. **1915** – Pressure at 162.5 psi. **1930** – Pressure at 162.3 psi. **1945** – Pressure at 161.9 psi. **2000** – Pressure at 161.6 psi. **2004** – Re-pressurize to 167.4 psi (5.33 gals in total). Let stabilize and left pressure on pipe overnight. **2030** – Secured for the day and left site.

**Willbros - Red Hill – Tank 5 Daily Notes Day 4**

6/26/14 – **0600** – Onsite. Sign in and Safety briefing. **0635** – Met with NAVFAC, Navy and Willbros personnel to discuss yesterday's actions and today's plan of work. **0725** – Descend into the lower tunnel to tank 5 and checked pressure gauges on 12" flange (for 18" line). **0735** – Ambient Temp: 79.9; Pipe Temp: 79.8 and Pressure was at 155.1 psi. **0802** – Ambient Temp: 79.9; Pipe Temp: 79.9 and Pressure was at 154.6 psi. **0830** – Inside tank Probe temp was 79.6. **0915** – Pressure at 153.5 psi. Pipe Temp: 79.9, and Ambient Temp: 79.9. We pressurized line to 170.1 psi. Closed off valve to the pipe and removed our test



**PIPELINE PETROLEUM SERVICES, INC.**

**Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI**

equipment from the pipe. We also took the filters off our pressure recorder and digital gauge and directly installed into the pipe to make sure there was no source of air in our test tree. Bleed air and let stabilize at **0945**. **0950** – Pressure at 163.9 psi. **1005** - Pressure at 163.5 psi. **1020** - Pressure at 163.3 psi. Inside tank Probe Temp: 79.7. **1025** – Line still losing pressure, bleed off pressure and stop all meters from running. **1035** - Switch out Aux temp recorder with crew inside the tank to move back to the 32" line. **1100** – Back in lower tunnel, activate our meters and set up our pressure recorder and digital gauge and directly installed into the 20" flange (for 32"line). **1115** – Crew inside of tank begin bleeding air from ported blind. **1138** – Start pressurizing line with water thru the pump. **1143** – Pressure at 48.1 psi (15.98 gals in total). **1147** – Start pressurizing line by using pump. **1150** – Pressure at 75.0 psi but decreasing. Got call from crew inside of the tank on radio. There are more leaks from 32" flange inside of tank. Bleed off pressure. **1155** – D. Cobb and James Hagen went to identify leaks in the tank. Attempt to tighten up bolts using knock wrenches. **1235** – Cut on water and pressurized the pipe thru the pump using only the main pressure. **1241** – Pressure at 48.0 psi (16.45 gals in total) **1242** – Start using the pump. **1244** – Pressure at 75.0 psi but decreasing. **1320** – Pressure at 64.0 psi. Start pressurizing. **1322** – Pressure at 75.0 psi (17.55 gals in total). Continue pumping. **1323** - Pressure at 87.5 psi (18.46 gals in total). Crew is still trying to tighten up bolts inside tank. **1327** - Pressure at 77.4 psi. Pressurize back up to 80.0 psi (19.16 gals in total). **1423** – Depressurize line – gasket is leaking from a triangle notch cut out of the flange inside of the tank. Drained out 5 gallons from line. Willbros crew went to get more material to make up thicker, more pliable gasket. **1520** – Drained out 5 gallons from line. **1545** – Crew makes up ¼ " gasket and install it on 32" flange inside tank. **1806** – Start filling up pipe with water thru the pump using water main pressure. **1815** – Pressure at 48.6 psi (10.25 gals in total). Stop the water. Bleed off pressure. **1824** – D. Cobb and James back in lower tunnel. Use the water to pressurize line thru the pump. **1838** – Pressure at 48.2 psi. (17.88 gals in total) Start pump up. **1857** – Pressure at 71.6 psi. (18.00 gals in total). We had to stop pumping and take the flow meter out and clean the turbine. **1907** – Place flow meter back in service and start pressurizing back up with pump. **1912** – Pressure at 165.0 psi (19.5 gals in total). Let stabilize. **1935** – Pressure at 163.0 psi. **1950** – Pressure at 162.5 psi. **1956** – Pressure at 162.2 psi. Bleed down to 152.2 psi for the DV / DP check. (910 mil drained out) **1958** – Pressure up line to 168.1 psi. (0.15 gals added in) **2000** – **START TEST**. Take readings every 15 mins for the 1<sup>st</sup> hr and 30 mins thereafter. (See gauge sheet). **2400** – **TEST COMPLETE**. Leave pressure on line over night because line never fully stabilized, even though the rate of decrease slowed. **0045** – Secure for the day and Left site.

**Willbros - Red Hill – Tank 5 Daily Notes Day 5**

**6/27/14** – **0900** – Onsite. Sign in and Safety briefing. Met with Willbros personnel to discuss today's plan of work. **0915** – Descend into lower tunnel to tank 5 and checked pressure gauges on 20" flange (for 32" line). **0930** – Ambient Temp: 79.9; Pipe Temp: 79.9 and Pressure was at 162.3 psi. De-pressurize line and download data from dataloggers. Load up equipment in pelican case for shipping. **1020** – Mob to upper tunnel and secure tank. **1120** – Mob outside of upper tunnel. Review site actions over the past week. **1200** – Secure for the day. Left site.

PIPELINE PETROLEUM SERVICES, INC.

Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI

**APPENDIX C –**

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**TEST ID 14-332-01A DETAILED TEST RESULTS**

**TEST ID 14-332-01B DETAILED TEST RESULTS**

**TEST ID 14-332-02 DETAILED TEST RESULTS**

PIPELINE PETROLEUM SERVICES, INC.

Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI

**APPENDIX C –**

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**TEST ID 14-332-01A DETAILED TEST RESULTS**

**TEST ID 14-332-01B DETAILED TEST RESULTS**

**TEST ID 14-332-02 DETAILED TEST RESULTS**









Pipeline Pressure Test Report (Continued)

**VI: ATTACHMENTS TO THIS REPORT: (All May Not Be Included or Required)**

- |   |   |   |
|---|---|---|
| <input checked="" type="checkbox"/> Attachment A / Test Pressure Calculations                 | <input checked="" type="checkbox"/> Attachment F / Volume Change Calculations | <input type="checkbox"/> Pipeline Elevation Drawing               |
| <input checked="" type="checkbox"/> Attachment B / Pre-Test Calculations & Pressurization Log | <input type="checkbox"/> Attachment G / Test Procedure & Valve Line-Up Sheet  | <input checked="" type="checkbox"/> Pipeline Test Section Drawing |
| <input checked="" type="checkbox"/> Attachment C / Pressure / Volume Plot                     | <input type="checkbox"/> Attachment H / Loading Arm Information               | <input type="checkbox"/> Test Equipment Drawing                   |
| <input checked="" type="checkbox"/> Attachment D / Pressure & Temp Log                        | <input type="checkbox"/> Attachment I / Photograph Page(s)                    | <input type="checkbox"/> Disposal Manifest                        |
| <input checked="" type="checkbox"/> Attachment E / Pressure & Temperature Evaluation          |   |   |
|   | <input checked="" type="checkbox"/> Pressure Graph                            |   |
|   | <input checked="" type="checkbox"/> Temperature Graph                         |   |

**VII: GENERAL TEST REMARKS: (List General Pipeline Condition / Recommendations from Visual Inspection)**

Test considered inconclusive IAW applicable jurisdictional regulation, applied industry standards, and the intent of the test.  
 This is not a precision leak detection test and should not be considered as such. This hydrotest is considered a point-in-time, pressure decay, strength / stress / leak test against installed test blinds to determine if there are possible leaks of the stated MAOP / MAWP.  
 Test results are based on criteria established by (in Part) API-RP-1119; California State Fire Marshall Office (CSFM), as well as, calculated thermal pressure loss / gain, calculated volume loss / gain, no visual leaks identified in exposed piping during the test period, good engineering practice, and accepted industry practice. The pass/fail criteria may or may not be the required regulation however the criteria used is the accepted industry practice and is greater than or equal to the requirements in the jurisdictional regulation.

Initial pressurization attempted on 6/23/14 and the flange gasket inside of the tank began leaking at 60 psi when the pressurization pump was started. Attempts at tightening flange was unsuccessful. Remove flange and remove defective gasket. Install a rubber full faced gasket in conjunction with a new Garlok full faced gasket. Repressurize and this gasket combination began to leak at 75 psi. Remove flange for the second time and install two Garlok gaskets with high pressure / temperature silicone sealant between the flange face and gaskets and between the gaskets themselves.  
 The flange face is coated and uneven making proper sealing difficult. This combination leaked as well from a triangular notch that was cut out of the flange on the tank side of the pipe. The final configuration of a 1/4" thick neoprene gasket proved successful at sealing the flange for the test.

Interior of the pipe section was reported to be affected by corrosion pitting by the customer prior to our arrival and filling. This did not affect the test procedure and is added to this report only as additional information.

The line pressure never truly stabilized during the official test period, however the last 45 minutes of the following day (After the dataloggers were removed and the data recovered) appeared to achieve stabilization.  
 Evidence of the amount of trapped air in the line is the calculated volume to reach test pressure was approximately 1.7 gallons and it required over 19.4 gallons to reach test pressure which is equivalent to approximately 8.74% air by volume in the line.  
 We highly recommend a pneumatic test to confirm the existence of trapped air in the test section.

**VIII: TEST EQUIPMENT INFORMATION:**

(See drawing of testing apparatus if required and Calibration Certificates)

All calibrations are performed third-party and are traceable to NIST.

Equipment Description:	PPSI Unit Number:	Manufacturer:	Serial Number:	Calibration Date:	Calibrated By:
Pipe Pressure Datalogger	Unit 1	MadgeTech	N84154	4/11/2014	Madgetech
4 Channel Temperature Datalogger (Thermocouple)	Unit 1	MadgeTech	N82430	8/21/2013	Madgetech
2 Channel Temperature Datalogger (Thermocouple)	Aux Unit 1	MadgeTech	N84147	8/20/2013	Madgetech
Digital Flowmeter / Totalizer (1/2")	Unit 3	GPI Industries	3206877	6/16/2014	Angels Instruments
Digital Flowmeter / Totalizer (1")	Unit 4	GPI Industries	3710745	6/16/2014	Angels Instruments
0-5000 psi Digital Deadweight Accurate Test Gauge	Unit 1	Crystal	870422	5/5/2014	Angels Instruments

**IX: SIGNATURES**

<b>Tested By:</b> Dennis Cobb	<b>Report Prepared By:</b> Dennis Cobb	<b>Reviewed &amp; Approved:</b> Dennis Cobb	<b>Customer Witness:</b> James Hagen
<b>Title:</b> Vice President	<b>Title:</b> Vice President	<b>Title:</b> Vice President	<b>Title:</b> Project Manager
<b>Signed:</b> 	<b>Signed:</b> 	<b>Signed:</b> 	<b>Company:</b> Willbros Government Services
<b>Date:</b> 6/26/2014	<b>Date:</b> 6/26/2014	<b>Date:</b> 6/26/2014	<b>Signed: (If Required)</b>
			<b>Date:</b> 6/26/2014



# PIPELINE PETROLEUM SERVICES, INC.

## Piping Test Pressure Calculations (Attachment A)

Note: Green cells that are blank indicate a value of 0 (Zero).

Note: Fill in blue cells with required information / Green cells are calculated values.

<b>Test ID Number:</b>	14-332-01A	<b>Test Section:</b>	Tank 5 Fuel Piping - 32"
<b>Dwg Code Color:</b>	None	<b>Customer:</b>	Willbros Government Services
<b>Date:</b>	6/26/2014	<b>Location:</b>	Red Hill Fuel Farm
Oahu, HI			

### TEST CALCULATIONS INPUT

NPS	=	32.000	in.
D	=	31.250	in.
t	=	0.375	in.
W <sub>JF</sub>	=	0.8	
D <sub>F</sub>	=	0.72	
SMYS	=	35,000	psi
P <sub>WP</sub>	=	108.25	psi
G	=	1	
LE	=		feet
HE	=	9.5	feet
TE	=	9.24	feet
▲E	=	9.5	feet

- NPS = Nominal Pipe Size (Diameter Inches)
- D = Outside Diameter of pipe (in)(Avg of all sections x % total length)
- t = Pipe wall Thickness (in)(Avg of all sections x % total length)
- W<sub>JF</sub> = Weld Joint Factor (From Report Page 1)(Range (.6 - 1.0) per ASME B 31.4 Table 402.4.3)
- D<sub>F</sub> = Design Factor (From Report Page 1)(.72 for Haz Liquid Pipelines per ASME B31.4)
- SMYS = Specified Minimum Yield Strength (From Report Page 1)
- P<sub>WP</sub> = Maximum Working Pressure (psi)
- G = Product (Test Medium) Specific Gravity
- LE = Lowest elevation
- HE = Highest elevation
- TE = Test equipment elevation
- ▲E = Elevation Difference (If pipeline has an elevation difference >100' attach pipeline profile dwg)

**Describe How Elevations Determined:** (Line of sight estimation, known data, current survey, information source, ect.)  
 Foot of hydrostatic head was calculated at 9.5' based on 4 psi static head pressure x .433 psi / ft (=9.24') + 6" at bottom of pipe not recorded by the gauge due to location of the gauge itself relative to the center of the pipe.

### TEST PRESSURE CALCULATIONS RESULTS

Nominal Test Pressure: (PSI) 162.375

162.4	psi	Min. Pressure at High Point
166.5	psi	Max. Pressure at Low Point
162.5	psi	Pressure at Test Equipment Point
19.3%		Test Pressure as % SMYS
840.0	psi	100% SMYS
483.8	psi	Design Pressure (Calculated - Pipe Only)

**Calculate Max Low Point Pressure:**  
 (Factor .433 psi / ft for water or Total Ft x .433 (Specific Gravity: 1.0) or correct factor for other test medium):  
 Test Medium: Water  
 (Use Formula: p=.433(h)(SG) where p: Pressure / h: Head in Ft / SG: Specific Gravity Test Medium)  
 h: (Ft) 9.5  
 SG: 1

### TEST RESULTS

P <sub>MAX</sub>	=	168.0	psi
P <sub>MIN</sub>	=	164.9	psi
Difference	=	-3.1	psi

- P<sub>MAX</sub> = Maximum test gauge pressure
- P<sub>MIN</sub> = Minimum test gauge pressure

**Remarks & Assumptions:** We have to assume that the weld joint factor for this pipe is .08 for steel, however no data was available. We also have to assume that the design factor of .72 from ASME is the same because the line is in combustible liquid service.  
 Test pressure determined by max head from a full tank calculated by (.433)(SG)(Height) = 250' high x 1 (SG of water) x .433 = 108.25 x 1.5 = 162.375



PIPELINE PETROLEUM SERVICES, INC.

Pre-Test Calculations & Pressurization Log (Attachment B)

Note: Green cells that are blank indicate a value of 0 (Zero).  
Note: Fill in blue cells with required information / Green cells are calculated values.

Test ID Number: 14-332-01A      Customer: Willbros Government Services      Dwg Code Color: None  
 System Under Evaluation: Tank 5 Fuel Piping - 32"      Date: 6/26/2014      Location: Red Hill Fuel Farm

**Calculated DV / DP Data**

DV / DP (Change in Volume / Change in Pressure): DV / DP is defined as the change in volume for an associated change in pressure of a known volume under pressure. Two DV/DP calculations are used in these guidelines, a theoretical and a field value. A theoretical DV/DP will give the expected volume change for an associated change in pressure for the specified volume under test assuming that the volume under pressure is free of entrained gas. The field value of DV/DP is the actual volume change in pressure for the specified volume under test. If air exists within the line under pressure, this value will be different than the theoretical value.

**The theoretical DV/DP for aboveground (unrestrained) pipe is calculated through the following equation:**

$$\frac{DV}{DP} = V \cdot \left[ \left( \frac{D}{E \cdot t} \right) \left( \frac{5}{4} - \nu \right) + C \right]$$

**The theoretical DV/DP for buried (restrained) pipe is calculated through the following equation:**

$$\frac{DV}{DP} = V \cdot \left[ \left( \frac{D}{E \cdot t} \right) (1 - \nu^2) + C \right]$$

where,  
 V = volume of the segment for the individual pipe diameter, D (gallons),  
 D = outside diameter of pipe (in),  
 E = elastic modulus of steel pipe (psi),  
 t = wall thickness of pipe (in),  
 ν = poisson's ratio of steel pipe,  
 C = compressibility of test media (in<sup>3</sup>/in<sup>3</sup>/psi).

**NOTE:** For a test segment with multiple diameters, sum the individual DV/DP's of each pipe diameter to obtain a total DV/DP for the entire test section.

**Restrained Pipe (Underground)**  
(Volume = 0.0408 x d<sup>2</sup> x L)

V/A	1753.12
D=	31.25
E=	2.95E+07
t=	0.375
ν=	0.3
C=	3.11E-06
DV/DP=	0.009958816

Weight of Restrained Pipe: 0.92  
**AVG DV / DP for Test Section: (Gal)** 0.92  
 dV/dP: Change in volume with respect to pressure.

**Unrestrained Pipe (Aboveground & Inside)**  
(Volume = 0.0408 x d<sup>2</sup> x L)

V/A	39.84
D=	31.25
E=	2.95E+07
t=	0.375
ν=	0.3
C=	3.11E-06
DV/DP=	0.00463618

Weight of Unrestrained Pipe: 0.06  
**AVG DV / DP for Test Section: (Gal)** 0.06  
 dV/dP: Change in volume with respect to pressure.

**Use the Following Information for DV/DP Calculations - Values From Properties Charts Below**

Test Medium:	Water
B= Coef of Expansion:	1.23E-04
C=Compressibility of Test Media:	3.11E-06
Pipe Material #1:	Carbon Steel
E = Elastic Modulus of Pipe #1 (PSI):	2.95E+07
ν = Poisson's Ratio of Pipe #1:	0.3
α = Linear Coefficient of Expansion: Pipe #1:	6.10E-05
Pipe Material #2:	N/A
E = Elastic Modulus of Pipe #1 (PSI):	
ν = Poisson's Ratio of Pipe #1:	
α = Linear Coefficient of Expansion: Pipe #2:	
Number of Different Pipe Materials:	1
E Avg For Pipe Materials:	2.95E+07
ν Avg For Pipe Materials:	0.3
α Avg For Pipe Materials:	6.10E-05

**Property Chart for Pipe Material**

Pipe Material	Elastic Modulus: E	Coefficient of Expansion: α	Linear Coefficient of Expansion: α	Poisson's Ratio: ν
Carbon Steel	2.95E+07	6.50E-06	6.10E-06	.27-.30
Stainless Steel	2.8E+07	9.60E-06		.30-.31
FRP	2.3E+06	1.16E-05	1.16E-05	0.33
Aluminum	1.00E+07			0.33

**Property Chart for Test Medium**

Test Medium	Compressibility: C = (1/β)	Bulk Modulus: (β)	Coefficient of Expansion: B	SG @ 60°F
JP-8 / JP-8	5.85E-06	1.71E+05	4.98E-04	0.81
Diesel	5.21E-06	1.92E+05	4.69E-04	0.85
Gasoline	5.29E-06	1.89E+05	4.67E-04	0.84
Water	3.11E-06	3.22E+05	1.23E-04	1.00

**Test Sections**

Pipe Section (Identification)	Pipe Material	Nominal Pipe Ø (in)	Outside Ø (in)	Wall Thickness (in)	AVG Wall Thickness Exposed (AG)	AVG Wall Thickness Buried (BG)	AVG Wall Thickness Inside (IN)	dV/dT: Unrestrained (AG & IN) Pipe: V(A-B-C) Restrained (Buried) Pipe: V(B-C) (Total Last Cell)	Configuration Buried (UG) / Inside (IN)	Length (Ft)	Volume (Gallons)	Volume per Foot Pipe ID	Length AG (% Total Length)(Ft)	Length BG (% Total Length)(Ft)	Length Inside (% Total Length)(Ft)	Volume AG (% Total Length)(Ft)	Volume BG (% Total Length)(Ft)	Volume Inside (% Total Length)(Ft)	
Non Exposed	CS / STD	32	32	0.375		0.375		0.194	Buried	44	1753.12	39.84		44			1753.12		85.20
Nozzle Inside Tank	CS / STD	32	32	0.375			0.375	0.004	Inside	1	39.84	39.84			1				39.84
Nozzle Outside Tank	CS / STD	20	20	0.375			0.375	0.005	Inside	3	45.36	15.12			3				45.36
<b>Total # AG Pipe Sections:</b>						0.375	0.375	0.203		<b>48</b>	<b>1838.32</b>			<b>44</b>	<b>4</b>		<b>1753.12</b>		<b>85.20</b>
<b>Total # BG Pipe Sections:</b>		1				<b>0.375</b>							<b>95.67</b>					<b>19.44</b>	
<b>Total # IN Pipe Sections:</b>		2				<b>0.375</b>													
<b>Total # Pipe Sections:</b>		3																	
<b>Total Exposed Pipe Length: (AG &amp; IN)</b>			4	(Ft)															
<b>Total Non-Exposed Pipe Length: (UG)</b>			44	(Ft)															
<b>Total Exposed Volume: (AG &amp; IN)</b>																			85.20 (Gal)
<b>Total Non-Exposed Volume: (UG)</b>																			1753.12 (Gal)
<b>Total Volume to Fill Test Section (If Line Empty)(Gal):</b>																			1838.32
<b>Test Pressure (From Report Page 1)(PSI):</b>																			162.375
<b>Total Volume to Reach Test Pressure From 0 psi (Use DV / DP Chart Below)(Gal):</b>																			1,687.21







PIPELINE PETROLEUM SERVICES, INC.

Theoretical DV/DP (Test Pressure Fill Chart)(0-453 psi)

Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)
1	0.010462436	51	0.53307417	101	1.0659689	151	1.578317627	201	2.100339307	252	2.634013523	302	3.179623254	352	3.73709984	403	4.312123154
2	0.020904669	52	0.5435266	102	1.08614833	152	1.598770091	202	2.111391792	252	2.634013523	302	3.179623254	352	3.73709984	403	4.312123154
3	0.031357304	53	0.55397903	103	1.07660077	153	1.59922498	203	2.121844227	253	2.644466957	303	3.180076788	353	3.73709984	404	4.312123154
4	0.041810938	54	0.56443147	104	1.0870532	154	1.609674841	204	2.132296661	254	2.654920411	304	3.180530242	354	3.73709984	405	4.312123154
5	0.052262173	55	0.5748838	105	1.09750563	155	1.620127365	205	2.142749096	255	2.665373865	305	3.180983696	355	3.73709984	406	4.312123154
6	0.062714608	56	0.58533624	106	1.10795807	156	1.6305798	206	2.153201531	256	2.675827319	306	3.18143715	356	3.73709984	407	4.312123154
7	0.073167042	57	0.59578867	107	1.1184105	157	1.64103224	207	2.163653965	257	2.686280773	307	3.181890604	357	3.73709984	408	4.312123154
8	0.083619477	58	0.6062411	108	1.12886294	158	1.651484659	208	2.174106399	258	2.696734227	308	3.182344058	358	3.73709984	409	4.312123154
9	0.094071912	59	0.61669354	109	1.13931537	159	1.661937104	209	2.184558934	259	2.707187781	309	3.182797512	359	3.73709984	410	4.312123154
10	0.104524346	60	0.62714598	110	1.14976781	160	1.672389538	210	2.195012329	260	2.717641225	310	3.183250966	360	3.73709984	411	4.312123154
11	0.114976781	61	0.63759831	111	1.16022024	161	1.682841973	211	2.205464773	261	2.72809467	311	3.18370442	361	3.73709984	412	4.312123154
12	0.125429215	62	0.64805065	112	1.17067268	162	1.693294408	212	2.215917218	262	2.738548114	312	3.184157874	362	3.73709984	413	4.312123154
13	0.13588165	63	0.65850308	113	1.18112511	163	1.703746842	213	2.226369653	263	2.748991559	313	3.184611326	363	3.73709984	414	4.312123154
14	0.146334085	64	0.66895552	114	1.19157755	164	1.714199277	214	2.236822097	264	2.759435004	314	3.185064778	364	3.73709984	415	4.312123154
15	0.156786519	65	0.67940796	115	1.20203009	165	1.724651711	215	2.247274542	265	2.769878449	315	3.18551823	365	3.73709984	416	4.312123154
16	0.167238954	66	0.6898604	116	1.21248252	166	1.735104146	216	2.257726986	266	2.780321894	316	3.185971682	366	3.73709984	417	4.312123154
17	0.177691388	67	0.70031296	117	1.22293496	167	1.745556581	217	2.26817943	267	2.790765339	317	3.186425134	367	3.73709984	418	4.312123154
18	0.188143823	68	0.7107654	118	1.23338739	168	1.756009015	218	2.278631875	268	2.801208784	318	3.186878586	368	3.73709984	419	4.312123154
19	0.198596258	69	0.72121784	119	1.24383982	169	1.76646145	219	2.28908431	269	2.811652229	319	3.187332038	369	3.73709984	420	4.312123154
20	0.209048692	70	0.73167028	120	1.25429226	170	1.776913884	220	2.299536746	270	2.822095674	320	3.18778549	370	3.73709984	421	4.312123154
21	0.219501127	71	0.74212272	121	1.26474469	171	1.787366319	221	2.309989182	271	2.832539119	321	3.188238942	371	3.73709984	422	4.312123154
22	0.229953562	72	0.75257516	122	1.27519713	172	1.797818754	222	2.320441617	272	2.842982564	322	3.188692394	372	3.73709984	423	4.312123154
23	0.240406	73	0.7630276	123	1.28564956	173	1.808271189	223	2.330894052	273	2.85342601	323	3.189145846	373	3.73709984	424	4.312123154
24	0.250858431	74	0.7734801	124	1.29610199	174	1.818723623	224	2.341346487	274	2.863869456	324	3.189599298	374	3.73709984	425	4.312123154
25	0.261310866	75	0.78393254	125	1.30655443	175	1.829176058	225	2.351798922	275	2.874312901	325	3.19005275	375	3.73709984	426	4.312123154
26	0.2717633	76	0.79438498	126	1.31700686	176	1.839628492	226	2.362251357	276	2.884756347	326	3.190506202	376	3.73709984	427	4.312123154
27	0.282215735	77	0.80483742	127	1.32745929	177	1.850080927	227	2.372703792	277	2.895199792	327	3.190959654	377	3.73709984	428	4.312123154
28	0.29266817	78	0.81528986	128	1.33791173	178	1.860533361	228	2.383156227	278	2.905643237	328	3.191413106	378	3.73709984	429	4.312123154
29	0.303120604	79	0.8257423	129	1.34836416	179	1.870985796	229	2.393608662	279	2.916086682	329	3.191866558	379	3.73709984	430	4.312123154
30	0.313573038	80	0.83619477	130	1.3588166	180	1.881438231	230	2.404061097	280	2.926530127	330	3.19232001	380	3.73709984	431	4.312123154
31	0.324025473	81	0.84664721	131	1.36926903	181	1.891890665	231	2.414513526	281	2.936973572	331	3.192773462	381	3.73709984	432	4.312123154
32	0.334477908	82	0.8571	132	1.37972147	182	1.9023431	232	2.424965961	282	2.947417017	332	3.193226914	382	3.73709984	433	4.312123154
33	0.344930342	83	0.86755247	133	1.3901739	183	1.912795534	233	2.435418396	283	2.957860462	333	3.193680366	383	3.73709984	434	4.312123154
34	0.355382777	84	0.87800491	134	1.40062634	184	1.923247969	234	2.445870831	284	2.968303907	334	3.194133818	384	3.73709984	435	4.312123154
35	0.365835212	85	0.88845735	135	1.41107878	185	1.933700404	235	2.456323266	285	2.978747352	335	3.19458727	385	3.73709984	436	4.312123154
36	0.376287646	86	0.89890979	136	1.42153121	186	1.944152838	236	2.466775699	286	2.989190797	336	3.195040722	386	3.73709984	437	4.312123154
37	0.386740081	87	0.90936223	137	1.43198365	187	1.954595273	237	2.477228134	287	2.999634242	337	3.195494174	387	3.73709984	438	4.312123154
38	0.397192515	88	0.91981467	138	1.44243609	188	1.965037707	238	2.487680569	288	3.010077687	338	3.195947626	388	3.73709984	439	4.312123154
39	0.40764495	89	0.93026711	139	1.45288853	189	1.975480142	239	2.498133002	289	3.02052114	339	3.196401078	389	3.73709984	440	4.312123154
40	0.418097385	90	0.94071955	140	1.46334097	190	1.985922576	240	2.508585437	290	3.030964595	340	3.19685453	390	3.73709984	441	4.312123154
41	0.428549819	91	0.95117199	141	1.47379341	191	1.99636501	241	2.51903787	291	3.041408042	341	3.197307982	391	3.73709984	442	4.312123154
42	0.439002254	92	0.96162443	142	1.48424585	192	2.006807446	242	2.529490315	292	3.051851489	342	3.197761434	392	3.73709984	443	4.312123154
43	0.449454688	93	0.97207687	143	1.49469829	193	2.017259881	243	2.539942754	293	3.062294936	343	3.198214886	393	3.73709984	444	4.312123154
44	0.459907123	94	0.98252931	144	1.50515073	194	2.027712315	244	2.550395193	294	3.072738383	344	3.198668338	394	3.73709984	445	4.312123154
45	0.470359558	95	0.99298175	145	1.51560317	195	2.03816475	245	2.560847632	295	3.08318183	345	3.19912179	395	3.73709984	446	4.312123154
46	0.480811992	96	1.00343419	146	1.52605561	196	2.048617184	246	2.571297071	296	3.093625277	346	3.199575242	396	3.73709984	447	4.312123154
47	0.491264427	97	1.01388663	147	1.53650805	197	2.059069619	247	2.58174951	297	3.104068724	347	3.200028694	397	3.73709984	448	4.312123154
48	0.501716861	98	1.02433907	148	1.54696049	198	2.069522054	248	2.592201949	298	3.114512171	348	3.200482146	398	3.73709984	449	4.312123154
49	0.512169296	99	1.03479151	149	1.55741293	199	2.080000000	249	2.602654388	299	3.124955718	349	3.200935598	399	3.73709984	450	4.312123154
50	0.522621731	100	1.04524434	150	1.56786537	200	2.090499223	250	2.613106827	300	3.135409265	350	3.20138905	400	3.73709984	451	4.312123154



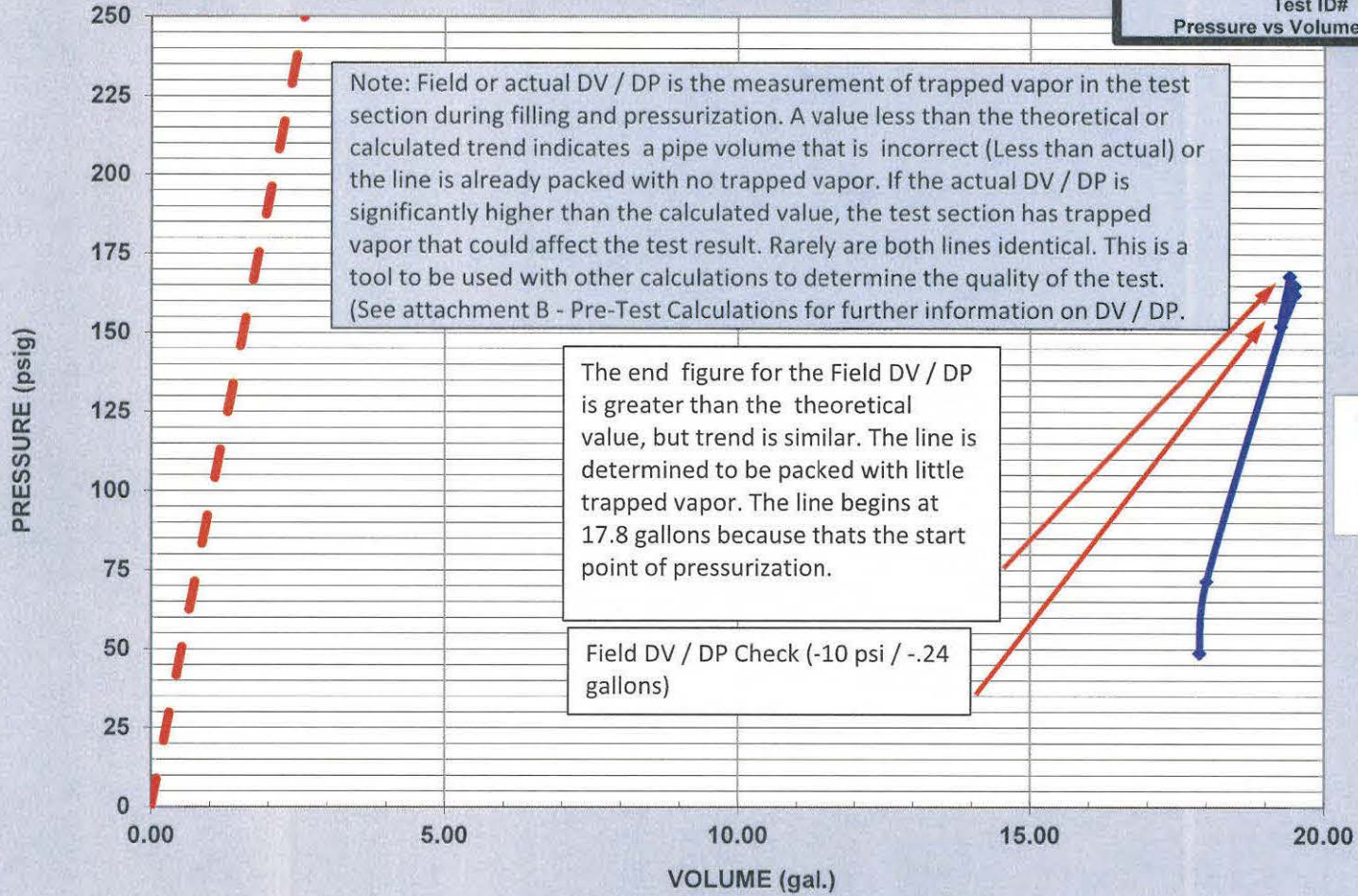
**PIPELINE PETROLEUM SERVICES, INC.**

Red Hill Underground Fuel Facility , HI

Tank 5 - 32" Line - F-76

Test ID# 14-332-01A

Pressure vs Volume Chart / Attachment C







**PIPELINE PETROLEUM SERVICES, INC.**

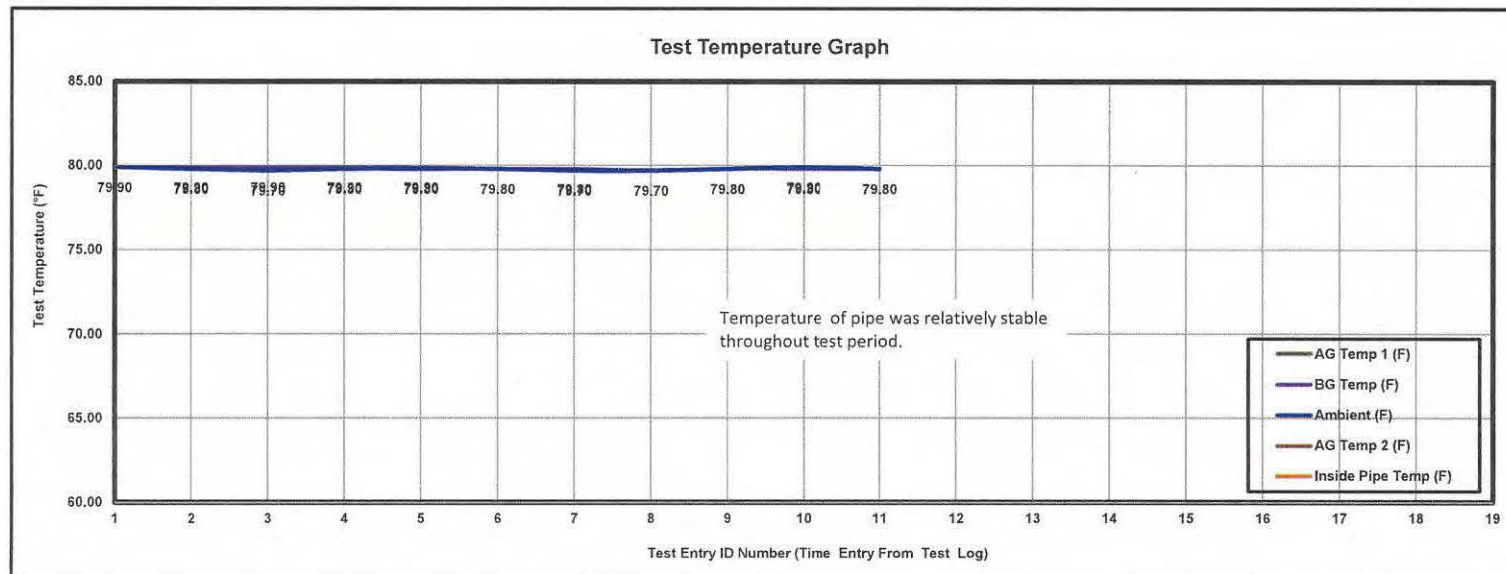
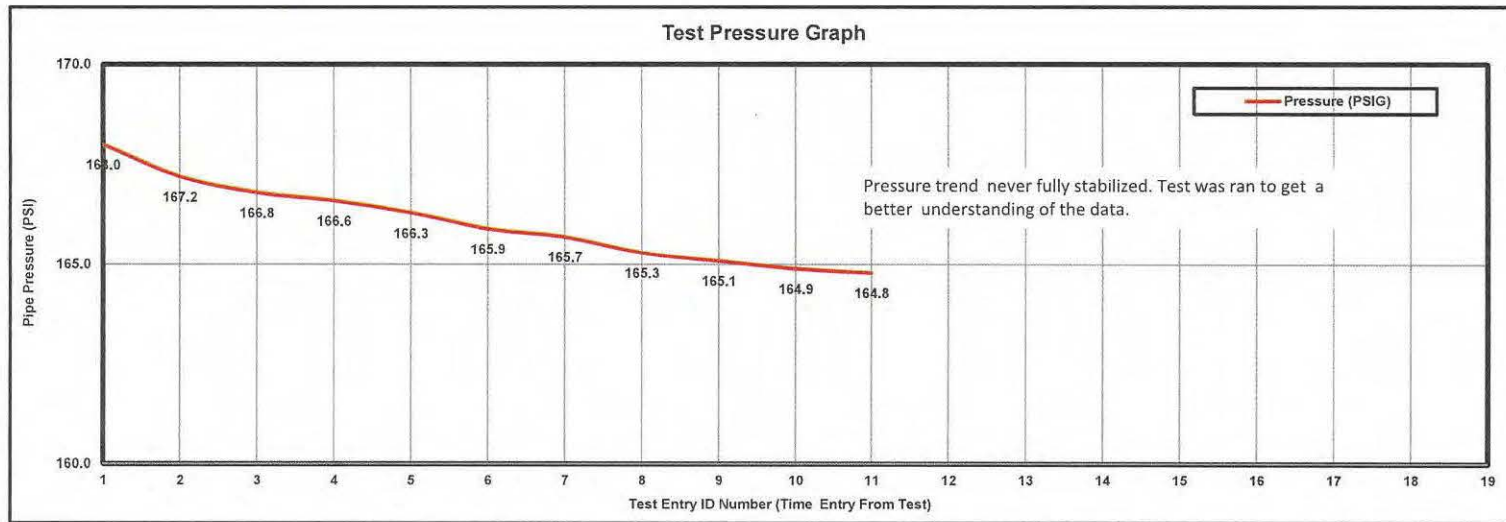
**Pipeline Pressure & Temperature Log (Attachment D)**

Date: 6/26/2014  
 Test ID No: 14-332-01A  
 Dwg Color Code: N/A

Note: Enter readings every 15 minutes for first hour of test (Entries 1-5) and every 30 minutes for each hour thereafter.

Customer: Willbros Government Services  
 Location: Red Hill Fuel Farm  
 System: Tank 5 Fuel Piping - 32"

Pressure Location & Unit #:		Location 1 & Unit #:		Location 2 & Unit #:		Location 3 & Unit #:		Location 4 & Unit #:		Number AG/IN Sensors:		Number BG Sensors:		Initial Pressurization From:		Remarks (Weather Conditions)		
Lower Yard Tunnel (Tank 5)		Lower Yard Tunnel (Tank 5)								1		1		48.7		PSI		
Entry ID Number	Time	Deadweight Pressure (psi)	Chart / Gauge Pressure (psig)	Aboveground / Exposed Pipe Temp (F) Location 1	Belowground / Non-Exposed Pipe Temp (F) Location 1	Aboveground / Exposed Pipe Temp (F) Location 2	Belowground / Non-Exposed Pipe Temp (F) Location 2	Aboveground / Exposed Pipe Temp (F) Location 3	Belowground / Non-Exposed Pipe Temp (F) Location 3	Aboveground / Exposed Pipe Temp (F) Location 4	Belowground / Non-Exposed Pipe Temp (F) Location 4	Inside Pipe Temp (F)	Ambient Temp (F)	Volume Added (Gal)	Volume Drained (Gal)	Percent Cloud Cover (0-100%)		
1	2000	168.0	*	79.90	79.90								79.90				Start Test	Time: 2000
2	2015	167.2		79.90	79.90								79.80				No weather effects - all piping is not exposed to the elements.	
3	2030	166.8		79.90	79.90								79.70					
4	2045	166.6		79.90	79.90								79.80					
5	2100	166.3		79.90	79.90								79.80					
6	2130	165.9		79.80	79.80								79.80					
7	2200	165.7		79.80	79.80								79.70					
8	2230	165.3		79.70	79.70								79.70					
9	2300	165.1		79.80	79.80								79.80					
10	2330	164.9		79.80	79.80								79.90					
11	2400	164.8		79.80	79.80								79.80					
12																		
13																		
14																		
15																		
16																		
17																		
18																		
19																		
Final		164.8		79.80	79.80								79.80				End Test	Time: 2400
Net Change		PSI Diff		Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Total Added	Total Drained	Note: Average Temperatures are used in the calculations for the press / temp eval sheet and volume change calculations.		
		-3.2		-0.10	-0.10								-0.10					
Average AG/IN Temp Start:				79.90		Average AG/IN Temp End:				79.80		Average Temperature for Tes: AG/IN:		79.85		Net Volume Loss(+) / Gain (-):		
Average BG Temp Start:				79.90		Average BG Temp End:				79.80		Average Temperature for Tes: BG:		79.85				
Equivalent Pressure Loss From Drained Amount: (Field DP / DV)(Hydrotest Only)						PSI Diff + PSI / Gal Equivalent from Drained Product (Calculated) = Total Pressure Differential (TPD)												
1		Gallons =		41.87		PSI		TPD =		-3.20		(Use on Evaluation Sheet - Attachment E)(Hydrotest Only)						
		Total Gal Drained =				PSI												
<b>Remarks: (Explanation of Any Pressure Discontinuities)</b>																		
* See attached recorder chart. Average AG Temperature includes both Inside and Aboveground / Exposed Temperatures, (if needed)																		
Used the same temperatures for AG & BG pipe from the dataloggers in the tunnel and inside of the tank because there was no practical way to actually measure the temperature of the piping as it was encased in concrete. Due to the non-exposed nature of all of the piping we feel the temperatures should be very close to each other given the amount of stabilization time allowed.																		
Left pressure on the line from 1200 AM (Pressure 164.8 psi / Pipe temp: 79.07 + 79.1) to 0930 AM the next morning (June 27) and the pressure was at 163.4 psi with a pipe temperature of 79.34+ 79.716.																		
Note: Line never fully stabilized.																		







# PIPELINE PETROLEUM SERVICES, INC.

## Hydrostatic Test Pressure and Temperature Evaluation Form (Attachment E)

Test ID Number: 14-332-01A		Dwg Color Code: None		Date: 6/26/14				
Customer: Willbros Government Services			Location: Red Hill Fuel Farm					
System Under Evaluation: Tank 5 Fuel Piping - 32"								
<b>Test Data:</b>								
Test Medium: (Water, Diesel, Gasoline, JP-5, JP-8, Kerosene, Other):		Water		IN: Inside Pipe Temp				
Pipeline Total Length: ("L"): (All Test Sections)		48		AG: Aboveground Pipe Temp				
Pipe Outside Diameter: ("D"): (Average From All Test Sections)		31.250		BG: Below Ground Pipe Temp				
Pipe Wall Thickness: ("t"): (Average From All Test Sections)		0.375		TL: Total Length				
D/t Ratio: (Pipe Ø / "t"): (Average From All Test Sections)		83.33		▲ P: Pressure Change				
Pipeline Total Volume: (From Report Page 1)		1838.32		▲ T: Temperature Change				
Beginning Test Pressure: ("Pb"):		168		Ending Test Pressure: ("Pe"):				
				164.8				
Observed Pressure Change (Attachment A): (Change P observed = Pe - Pb):				-3.2				
				▲ P (PSI)				
Beginning Test Temperature AG: ("Tb AG"):		79.90		Ending Test Temp AG: ("Te AG"):				
				79.80				
Length AG:		44		Percent Total Length: (Length AG / Total Length): % TL AG:				
				92%				
Beginning Test Temperature BG: ("Tb BG"):		79.90		Ending Test Temp BG: ("Te BG"):				
				79.80				
Length BG:		4		Percent Total Length: (Length BG / Total Length): % TL BG:				
				8%				
Beginning Test Temperature Inside: ("Tb IN"):				Ending Test Temp IN: ("Te IN"):				
Length IN:				Percent Total Length: (Length IN / Total Length): % TL IN:				
▲ T-AG: (Chg T=Te -Tb)		-0.10		x %TL AG: = Adjusted Average AG ▲ T:				
▲ T-BG: (Chg T=Te -Tb)		-0.10		x %TL BG: = Adjusted Average BG ▲ T:				
▲ T-IN: (Chg T=Te -Tb)		8%		x %TL IN: = Adjusted Average IN ▲ T:				
(Final (FChg T) = Adjusted Avg AG ▲ T + Adjusted Avg BG ▲ T + Adjusted Avg IN ▲ T / 3)				FChg T: -0.08				
				▲ T (° F)				
Average Temp (T avg)		(Tb AG + Tb BG + Tb IN) / 3 = 76.20		Tb Note: IN & AG are averaged together based on weighting factors.				
		(Te AG + Te BG + Te IN) / 3 = 76.10		Te				
Average Fluid / Pipe Temperature (T avg = (Te + Tb) / 2):		T avg: 76.15		(For Test Duration)				
Using T avg and D/t, find dP / dT from temperature compensation charts (exhibit 100,101,102, 103, 104, or 105) or calculate for the appropriate test medium:								
dP / dT = 19.44		psi / ° F From Pre-Test Calculations - Attachment B						
Formula for dP / dT Chart Development or Calculation used in Attachment B:								
dP = [B-2a] / [Dx(1-v²)/Et+C]		Formula and Results Validated by UFC 3-460-03 Section 9-3.5 / Pressure Relief Valves and CA State Hydrostatic Testing Worksheet. (Different Formula Variation)						
T		C=Compressibility factor for water (Or other test med), cu in/cu in/psig						
dP=psig change per degree C or F		a=Coefficient of expansion for steel,						
B=Coefficient of expansion of test medium		t=Pipe wall thickness, in						
D=Pipe OD in inches		T=Temperature, degrees C or F (20°C)(Or Tavg for test duration above)						
E=Modulus of elasticity for pipe material		Note: Modulus of Elasticity = Young's Modulus = Elastic Modulus						
v=Poisson's ratio, 0.3 for steel pipe								
Test Medium: Water		B= 1.23E-04		Bulk Modulus (β): 321,543				
		C= (1/β) 3.11E-06		(Reciprocal of the Bulk Modulus (β) in lb/in²)				
Pipe Material #1: Carbon Steel		E= 2.95E+07		a = 6.50E-06				
Pipe Material #2: N/A		E=		a =				
Pipe Material #3: N/A		E=		a =				
List all Pipe Material & Test Medium Assumptions Made for Test Calculations: The type and grade of pipe material was assumed because no hard data was available from the original construction of the facility.								
Test Variables for Calculations (Pipe Material Physical Properties from (in part) Appendix C, ASME B 31.3)								
Pipe Material	E	a (in/in/°F)	α (Linear)	Test Medium	C = (1/β)	Bulk Modulus (β):	B (° F)	SG @ 60°F
Carbon Steel	2.95E+07	6.50E-06	6.10E-06	JP-5 / JP-8 / Jet-A / Kerosene	5.18E-06	1.93E+05	4.98E-04	0.81
Stainless Steel	2.8E+07	9.60E-06		Diesel - LSD / ULSD / Dyed	5.21E-06	1.92E+05	4.59E-04	0.85
FRP	2.3E+06	1.16E-05		Gasoline	5.29E-06	1.89E+05	4.57E-04	0.84
Aluminum	1.00E+07			Water	3.11E-06	3.22E+05	1.23E-04	1.00
Other				Other				
Calculate the expected pressure change: Chg P expected = dP / dT x FChg T								
Figure corrected for various diameters of pipe within test section.								
Chg P expected =		dP / dT		FChg T				
(°C converted to °F)		19.44		(psi / °F) x -0.08				
				°F = -1.63				
				psi - Expected ▲ P				
Pressure increases (Chg P > 0): If Chg P observed > Chg P expected test is successful.								
Pressure decreases (Chg P < 0): If Abs (Chg P observed) < Abs (Chg P expected) test is successful.								
Test Successful: (Pass / Fail):		Fail		Expected ▲ P: (Calculated Chg P)				
				-1.6333				
Total pressure differential (TPD) from Attachment A (Log Sheet) →				Observed ▲ P: (From Log Sheet)				
				-3.2000				
Note: The sign (+/-) of the observed pressure change should be consistent with the sign of the temperature change (FChg T).								



PIPELINE PETROLEUM SERVICES, INC.

Hydrostatic Test Volume Change Calculations (Attachment F) Page 1 of 2							
Test ID Number:	14-332-01A			Dwg Code Color:	None		
Customer:	Willbros Government Services			Date:	6/26/2014		
System Under Evaluation:	Tank 5 Fuel Piping - 32"			Location:	Red Hill Fuel Farm		
<b>Volume Change Calculations for Pipeline Hydrostatic Test (Calculated Volume/Pressure Slope Method)</b>							
Standard Formula:	$\Delta V / V = Kp \Delta P + Kt \Delta T$			Where:	$Kp = [(Dn)(5/4 - \mu) / E] + 1/\beta = (1.9D / 2Et) + 1/\beta$		
$\Delta P$ = Liquid Pressure Change				And:	$Kt = 3a - g$		
$\Delta T$ = Liquid Temperature Change				L = Pipe Length	t = Pipe Wall Thickness		
$\Delta V$ = Liquid Volume Added to Inside of Pipe (Negative if Flows Out)				$\mu$ = Poisson's Ratio = 0.3	E = Young's Modulus = 30x10 <sup>6</sup> psi		
V = Nominal Pipeline Volume ( $\pi D^2 L / 4$ )				$\beta$ = Liquid Bulk Modulus, a function of Press & Temp	g = Liquid Volumetric Expansion Coefficient, a Function of Press & Temp		
D = Inside Pipe Diameter				a = Linear Coefficient of Thermal Expansion	Note: Modulus of Elasticity = Young's Modulus = Elastic Modulus		
Test Medium:	Water				Pipe Material:	Carbon Steel	
API Gravity (141.5/SG)-131.5	Specific Gravity SG 141.5/(131.5-Degrees API)	p (SG x 1000)	(Liquid Coefficient of Expansion) B & g =	Compressibility: C = (1/B)	(Young's Modulus) E=	Linear Coefficient of Expansion: a=	
10.00	0.9990	999.012	1.23E-04	3.11E-06	2.95E+07	6.50E-06	
Pipe Data		Test Date		6/26/2014	API Gravity	10.00	
Pipe Segment	$\phi$ Outside (in)	$\phi$ Inside (in)	Wall (in)	Length (Ft)	Volume (Gal)	Configuration	
Non Exposed	32	31.250	0.375	44	1753.12	Buried	
Nozzle Inside Tank	32	31.250	0.375	1	38.84	Inside	
Nozzle Outside Tank	20	19.250	0.375	3	45.36	Inside	
				Totals	48	1838.32	
Weighting for Pipeline Segment	% Total Length	Configuration			Buried	Exposed	Inside
Non Exposed	0.95	Buried			0.95		
Nozzle Inside Tank	0.02	Inside					0.02
Nozzle Outside Tank	0.02	Inside					0.02
Sum of Factors				Weight Factors	0.95		0.05
The above factors are used for weighting segment temperatures.							
<b>Corrected Temperatures</b>							
<b>Initial Test Temperatures</b>							
Buried	Exposed	Inside	Initial Corrected T1	DT1	AVG. T		
79.9	79.9		76.20	16.1900118	76.15		
<b>Final Test Temperatures</b>							
Buried	Exposed	Inside	Final Corrected T2	DT2			
79.8	79.8		76.10	16.0946465			
<b>Corrected Temperature Difference</b>							
				-0.10			
<b>Test Pressure Difference</b>							
Initial Pressure P1	Final Pressure P2	dPressure					
188	164.8	-3.2					
Calculate $(Kp) = (1.9D/2Et) + 1/\beta$ weighted value							
Calculating $C_{PL}$		$Kp (1/P)$					
$C_{PL} = 1/(1-F_p/P)$ or $Kp (1/P) =$		1.0006114	1.0005996				
Calculate $(Kt) = (3a - g)$ a-constant							
Calculating $C_{TL}$		$C_{TL} 1$	$C_{TL} 2$	Coefficient Of Linear Expansion	Temperature Correction Factor (c)	Test Duration	
$C_{TL} = \text{Exp}(-\alpha_{avg} DT * (1 + 0.8 \alpha_{avg} (DT + t_{avg})))$ or $Kt(1/F) =$		0.9946333	0.9946650	a	$\alpha_{avg}$	Hours	
				6.50E-06	3.31E-04	4.00	
<b>Calculating Fluid Volume Gain / Loss</b>							
$dV = V2 - V1 = V0((C_{PL}^2 C_{TL}^2) - V0(C_{PL}^1 C_{TL}^1))$		$dV = \text{Total Pipeline Volume} * (Kp * dP + Kt * dT)$		Net Volume Removed (Accountable Loss (-) / Gain (+) - From Log Sheet)		Unaccountable Loss	Actual Gain(+) / Loss(-)
Volume Loss/8hrs	-0.04	+		=		-0.04	
Volume Loss/hour	0.00	+		=		0.00	
Added or Subtracted During Test							
<b>CSFM Loss Allowable</b>							
Gal./hour	1.03	Gal./8hours	8.22				







**Pipeline Pressure Test Report - Test Summary**

Form Revision Number: 6  
 Form Revision Date: 4-Jan-14



Note: Green cells that are blank indicate a value of 0 (Zero).  
 Note: Fill in blue cells with required information / Green cells are calculated values.

I. GENERAL TEST INFORMATION															
Test ID No:	14-332-01B	Job No:	14-332	Type of Test:	Hydrostatic Pressure Decay <small>(Hydrostatic x 150% MAWP, Hydraulic x 125% or 150% MAWP)</small>	Minimum Test Duration: (Hrs)	4								
Date:	6/27/2014	Customer:	Willbros Government Services	<small>(Hydro-Pneumatic x 110% or 150% MAWP, Pneumatic x 110% MAWP)</small>		Dwg Color Code:	None								
Contract Number:	Willbros Contract # N62583-08-D-0132/003	System:	Tank 5 Fuel Piping - 32"	Location:	Red Hill Fuel Farm Oahu, HI										
Test Medium:	Water	Tank #:	5	AST / UST:	UST	Product:	Water								
Test Medium Source:	Water Line in Lower Access Tunnel	Specific Gravity:	141.5/(131.5 + Degrees API)	1	API Gravity:(141.5/SIS)-131.5	10.00	Flash Point:	N/A							
Test Medium Additives:	None	Included Pipe Sections or Laterals: (Test Section)	32" - F-76 service lateral to Tank 5 from the 20" flange at the wall of the Lower Access Tunnel to the 32" flange inside of the tank where the diverter was connected. (Diverter removed for the test)			Test Connection: (Location / Size / Type)	Ported test blind on the 20" flange located in the lower yard tunnel. Temp probe also placed inside of tank.								
Time Zone:	Hawaii	Country:	USA	Purpose of Test:	Annual Or Five-Year Requalification, New Commissioning, Post Repair, Other	Possible Suspected Leak									
Test Criteria: (Jurisdictional Regulation)	49 CFR 195.300 / CSFM / UFC 3-460-03					Skills Installed:	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No							
Test Procedure:	API RP-1110 / CSFM Guidelines / 49 CFR 195					Location(s): (List valve / tank number / ect.)	Size:								
Test Medium Disposal:	<input type="checkbox"/> Yes	<input checked="" type="checkbox"/> No	Disposal Company:	N/A	Valves and diffusers removed and test blinds installed.										
Disposal Type & Amount (Gals):	Willbros will drain pipeline into portable totes for disposal outside of the tunnel.														
II. PIPE DESIGN DATA															
System Design Data Code:	UNK - Assume ASME B31.3														
Pipe Specification:	UNK - Assume API 5L ERW														
Pipe Grade: (Pipe Grade A & B / Strength X42 - X60)	UNK					SMYS: (psi)	35,000	Pipe Information Source:	No pipe information was readily available from the facility.						
Year Installed:	Circa 1943														
Known Repairs / Modifications:	Date:			Known Repairs / Modifications:			Date:								
None known															
W <sub>JF</sub> (Weld Joint Factor)	0.8	(Range (.6 - 1.0) per ASME B 31.4 Table 402.4.3) / Source:					Assumption								
D <sub>F</sub> (Design Factor)	0.72	(72 for Haz Liquid Pipelines per ASME B31.4 or State Other Criteria):					N/A								
III. TEST SECTIONS (If Loading Arm Present in Test Section Include Total Length & Volume from attachment I)															
Pipe Section (Identification)	MP To (Location)	MP From (Location)	Nominal Pipe Ø (in)	Wall Thickness (in)	Outside Ø (in)	Inside Ø (in)	Pipe Material	Configuration (Buried-BG / Exposed-AG / Inside IN)	Length (Ft)	Section as % Total Pipe Length	Volume (Gallons)	Volume per Foot Pipe ID (Gal)	Length AG (%)(Ft)	Length BG (%)(Ft)	Length Inside (%)(Ft)
Non Exposed			32	0.375	32.000	31.25	CS / STD	Buried	44.0	91.67%	1753.12	39.84			
Nozzle Inside Tank			32	0.375	32.000	31.25	CS / STD	Inside	1.0	2.08%	39.84	39.84		44.0	1.0
Nozzle Outside Tank			20	0.375	20.000	19.25	CS / STD	Inside	3.0	6.25%	45.36	15.12			3.0
Total Pipe Sections in Test Section:			3	Averages:	0.375	31.250	27.250	Sum Of Factors:	1.00	Weight Of Factors: (=100%)			0.92	0.08	
Total Volume Test Section (Gal):			1838.32	Total Volume Test Section (CF):	245.76	Total Length Test Section: (Ft)	48.0	Total Length AG / BG / Inside: (ft)					44.0	4.0	
Use Factoring For Volume Change & Pressure / Temperature Calculations												Total Number Factors:		2	



Pipeline Pressure Test Report (Continued)

IV. TEST PRESSURE INFORMATION																	
Test Pressure:(psi)	162.375		% SMYS:	19.33%	MAWP: (psi)	108.25		Stated MAOP:(psi)	108.25		Max System Design Pressure: (100% SMYS x WJF x DF)(Pipe Only - Does Not Include Fittings & Components)	484					
How MAWP Determined: (Customer Provided / Pipeline Questionnaire / SPCC Plan / Calculated / Pump Deadhead / PRV Settings / Other):										Max head from a full tank calculated by (.433)(SG)(Height) = 250' high x 1 (SG of water) x .433 = 108.25 x 1.5 = 162.375							
Does pipeline have a elevation difference of 100' or greater? <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No					Pressure Relief Valves: <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No												
<i>(If yes then attach profile drawing of the pipeline indicating locations of pressure sensors IAW 49 CFR 195 if applicable)</i>																	
HP Elevation: (Ft)	9.5		Min Pressure @ High Point:	162.375	% SMYS:	19.33%											
LP Elevation: (Ft)			Max Pressure @ Low Point:	166	% SMYS:	19.82%											
Difference: (Ft)	9.5		Pressure at TE Elevation:	162	% SMYS:	19.33%											
Test Equipment (TE) Elevation: (Ft)	9.24		See Test Pressure Calculation Sheet														
Flange Class:	150 lb																
150 lb Class Flanges Max Test Pressure = 425 psi (MAOP: 275 psi) / 300 lb Class Flange Max Test Pressure = 1100 psi (MAOP: 720 psi)																	
Is Test Pneumatic or Hydro-Pneumatic? (Yes or No)			No			Joints / Welds Soaped? (Yes or No)			N/A								
<i>If Yes Use The Following Information if Test is Performed With Nitrogen:</i>																	
Estimated Volume of Nitrogen Needed From 0 psi to Test Pressure: (If Line Empty)(CF)			N/A			Equivalent Bottles:			N/A								
+ 1 ATM / 1 ATM = Volume CF of Nitrogen Needed (Note: 1 ATM = 14.7 psi)						Note: 1 Bottle = 300 CF											
Estimated Pipe Fill at Start of Pressurization: (%) (Existing product)						N/A											
Estimated Volume of Nitrogen Needed: (At Estimated Line Fill)			N/A			Equivalent Bottles:			N/A								
V. TEST SUMMARY																	
Weather (Test Start):	Test Section Inside - Weather Not A Factor				Weather (Test End):	N/A				Weather Comments:	None						
<b>Note: Only Use Volume Calculations &amp; Temperature Evaluation for Underground Hydrostatic or Hydraulic Testing (Not Applicable 100% AG Pipe for Pneumatic or Hydro-Pneumatic Testing).</b>																	
Does Test Section Have UG Pipe? (Yes or No)			Yes														
Test Volume Calculation Summary: (See Attachment B)																	
Volume Calculated to Fill Pipeline: (DV / DP)(Gal)(If Empty)			1838.32			Actual Volume to Fill Pipeline: (Gallon)			1836.03								
Volume Calculated to Reach Test Pressure from 0 PSI: (Pipeline must be full)(From Pre-Test Calculation Page):			1.6972			Difference:			17.7128								
Actual Volume Required to Reach Test Pressure: (From Pre-Test Calculation Page):			19.41			Equivalent % Pipe Fill (At Pressurization >100% = Pipe Full)( <100% = Pipe has Trapped Vapor)			8.74%								
Test Volume Correction Calculation Summary: (See Attachment B)																	
AVG Calculated DV / DP for Test Section: (Gal / psi)			0.0104524			dP/dV = (1dV/dP) (From Pre-Test Calcs)(psi/gal) =			95.67 PSI / Gal								
dV/dP: Change in volume with respect to pressure.						dP/dV: Change in pressure with respect to volume.											
						dV/dT (From Pre-Test Calcs - Sum of all pipe sections)(gal*F) =			0.203 Gal / *F								
dV/dT: Change in volume with respect to temperature									dP/dT: =(dP/dV)x(dV/dT)(psi/*F)			19.44 PSI / *F					
dP/dT: Change in pressure with respect to temperature																	
Equivalent Pressure Loss From Drained Amount: (Calculated DP / DV)			1			Equivalent Pressure Loss From Drained Amount: (Field DP / DV)			N/A			41.67					
Gallons =			95.67			Gallons =			N/A			41.67					
Total Gal Drained =						Total Gal Drained =											
Pressure & Temperature Evaluation (From Attachment E)																	
Chg P expected =					Calculating Fluid Volume Gain / Loss (From Attachment F)												
$\frac{dP}{dT}$ (psi / *F) x $FChg T$ = $Chg P$					dV = Total Pipeline Volume * K <sub>1</sub> * dT + dV/dP * dP					Net Volume Removed (Accountable Loss(-) / Gain(+)) (From Log Sheet)		Unaccountable Loss					
(*C converted to *F)					Change of Pressure Expected $\Delta P$							Actual Gain(+)/ Loss(-)					
Pressure increases (Chg P > 0): If Chg P observed > Chg P expected test is successful.					Volume Loss/hrs					0.00		0.00					
Pressure decreases (Chg P < 0): If Abs (Chg P observed) < Abs (Chg P expected) test is successful.					Volume Loss/hour					0.00		0.00					
Test Successful: (Pass / Fail):					Expected $\Delta P$ : (Calculated Chg P)					0.00		0.00					
Total pressure differential (TPD) from Attachment A (Log Sheet) →					Observed $\Delta P$ : (From Log Sheet)					-0.1000							
Note: The sign (+/-) of the observed pressure change should be consistent with the sign of the temperature change (FChg T).																	
Test Acceptable: <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No						CSFM Loss Allowable			1.03 Gal./hour			8.22 Gal./8hours					
Test Readings Recap:						Test Conclusion IAW CSFM / hr			Pass			Test Conclusion IAW CSFM / 8 hrs			Pass		
(IAW Applicable Test Criteria & Regulation)																	
Start Test		Time:		845		Start Pressure:		163.5		Average AG/IN Temp Start:		79.34		Average BG Temp Start:		79.34	
End Test		Time:		930		End Pressure:		163.4		Average AG/IN Temp End:		79.34		Average BG Temp End:		79.34	
Any Leaks or Weeps Detected During Pressurization or Test Period:		<input checked="" type="checkbox"/> Yes <input type="checkbox"/> No				Difference:		-0.1		Difference:				Difference:			
Remarks & Leak Corrections (Include Repairs Made Prior To Test):																	
No visual leaks were identified on the test section after the 32" flange gasket inside of the tank was properly sealed. There was at least three periods of pressurization to allow for the gasket to be changed / replaced.																	



Pipeline Pressure Test Report (Continued)

**VI: ATTACHMENTS TO THIS REPORT: (All May Not Be Included or Required)**

- |   |   |   |
|---|---|---|
| <input checked="" type="checkbox"/> Attachment A / Test Pressure Calculations                 | <input checked="" type="checkbox"/> Attachment F / Volume Change Calculations | <input type="checkbox"/> Pipeline Elevation Drawing               |
| <input checked="" type="checkbox"/> Attachment B / Pre-Test Calculations & Pressurization Log | <input type="checkbox"/> Attachment G / Test Procedure & Valve Line-Up Sheet  | <input checked="" type="checkbox"/> Pipeline Test Section Drawing |
| <input checked="" type="checkbox"/> Attachment C / Pressure / Volume Plot                     | <input type="checkbox"/> Attachment H / Loading Arm Information               | <input type="checkbox"/> Test Equipment Drawing                   |
| <input checked="" type="checkbox"/> Attachment D / Pressure & Temp Log                        | <input type="checkbox"/> Attachment I / Photograph Page(s)                    | <input type="checkbox"/> Disposal Manifest                        |
| <input checked="" type="checkbox"/> Attachment E / Pressure & Temperature Evaluation          |   |   |
|   | <input checked="" type="checkbox"/> Pressure Graph                            |   |
|   | <input checked="" type="checkbox"/> Temperature Graph                         |   |

**VII: GENERAL TEST REMARKS: (List General Pipeline Condition / Recommendations from Visual Inspection)**

Test considered inconclusive IAW applicable jurisdictional regulation, applied industry standards, and the intent of the test.  
 This is not a precision leak detection test and should not be considered as such. This hydrotest is considered a point-in-time, pressure decay, strength / stress / leak test against installed test blinds to determine if there are possible leaks at the stated MAOP / MAWP.  
 Test results are based on criteria established by (in Part) APLRP-1110; 5th Edition, California State Fire Marshall Office (CSFM), as well as, calculated acceptable thermal pressure loss / gain, no visual leaks identified in exposed piping during the test period, good engineering practice, and accepted industry practice. The pass/fail criteria may or may not be the required regulation however the criteria used is the accepted industry practice and is greater than or equal to the requirements in the jurisdictional regulation.

Initial pressurization attempted on 6/23/14 and the flange gasket inside of the tank began leaking at 60 psi when the pressurization pump was started. Attempts at tightening flange was unsuccessful. Remove flange and remove defective gasket. Install a rubber full faced gasket in conjunction with a new Garlok full faced gasket. Re-pressurize and this gasket combination began to leak at 75 psi. Remove flange for the second time and install two Garlok gaskets with high pressure / temperature silicone sealant between the flange face and gaskets and between the gaskets themselves.  
 The flange face is coated and uneven making proper sealing difficult. This combination leaked as well from a triangular notch that was cut out of the flange on the tank side of the pipe. The final configuration of a 1/4" thick neoprene gasket proved successful at sealing the flange for the test.

Interior of the pipe section was reported to be affected by corrosion pitting by the customer prior to our arrival and filling. This did not affect the test procedure and is added to this report only as additional information.

The pipeline never truly stabilized during the official test period, however the last 45 minutes of the following day (After the dataloggers were removed and the data recovered) appeared to achieve stabilization.

We highly recommend a pneumatic test to confirm the existence of trapped air in the test section.

This was a theoretical test using data from the last 45 minutes of the datalogger data. The results are the same with a volume loss passing result and a temperature evaluation resulting in a failure however the results are much closer: +/- .1 psi loss.  
 No data was changed from the "A" test other than the data entered in the log sheet to manipulate the calculations.

**VIII: TEST EQUIPMENT INFORMATION:**

(See drawing of testing apparatus if required and Calibration Certificates)

All calibrations are performed third-party and are traceable to NIST.

Equipment Description:	PPSI Unit Number:	Manufacturer:	Serial Number:	Calibration Date:	Calibrated By:
Pipe Pressure Datalogger	Unit 1	MadgeTech	N84154	4/11/2014	Madgetech
4 Channel Temperature Datalogger (Thermocouple)	Unit 1	MadgeTech	N82430	8/21/2013	Madgetech
2 Channel Temperature Datalogger (Thermocouple)	Aux Unit 1	MadgeTech	N84147	8/20/2013	Madgetech
Digital Flowmeter / Totalizer (1/2")	Unit 3	GPI Industries	3206877	6/16/2014	Angels Instruments
Digital Flowmeter / Totalizer (1")	Unit 4	GPI Industries	3710745	6/16/2014	Angels Instruments
0-5000 psi Digital Deadweight Accurate Test Gauge	Unit 1	Crystal	870422	5/5/2014	Angels Instruments

**IX: SIGNATURES**

Tested By:	Dennis Cobb	Report Prepared By:	Dennis Cobb	Reviewed & Approved:	Dennis Cobb	Customer Witness:	James Hagen
Title:	Vice President	Title:	Vice President	Title:	Vice President	Title:	Project Manager
Signed:		Signed:		Signed:		Company:	Willbros Government Services
Date:	6/27/2014	Date:	6/27/2014	Date:	6/27/2014	Signed: (If Required)	
						Date:	6/27/2014



# PIPELINE PETROLEUM SERVICES, INC.

## Piping Test Pressure Calculations (Attachment A)

Note: Green cells that are blank indicate a value of 0 (Zero).

Note: Fill in blue cells with required information / Green cells are calculated values.

Test ID Number:	14-332-01B	Test Section:	Tank 5 Fuel Piping - 32"
Dwg Code Color:	None	Customer:	Willbros Government Services
Date:	6/27/2014	Location:	Red Hill Fuel Farm
Oahu, HI			

### TEST CALCULATIONS INPUT

NPS	=	32.000	in.
D	=	31.250	in.
t	=	0.375	in.
W <sub>JF</sub>	=	0.8	
D <sub>F</sub>	=	0.72	
SMYS	=	35,000	psi
P <sub>WP</sub>	=	108.25	psi
G	=	1	
LE	=		feet
HE	=	9.5	feet
TE	=	9.24	feet
▲E	=	9.5	feet

- NPS= Nominal Pipe Size (Diameter Inches)
- D = Outside Diameter of pipe (in)(Avg of all sections x % total length)
- t = Pipe wall Thickness (in)(Avg of all sections x % total length)
- W<sub>JF</sub> = Weld Joint Factor (From Report Page 1)(Range (.6 - 1.0) per ASME B 31.4 Table 402.4.3)
- D<sub>F</sub> = Design Factor (From Report Page 1)(.72 for Haz Liquid Pipelines per ASME B31.4)
- SMYS = Specified Minimum Yield Strength (From Report Page 1)
- P<sub>WP</sub> = Maximum Working Pressure (psi)
- G = Product (Test Medium) Specific Gravity
- LE = Lowest elevation
- HE = Highest elevation
- TE = Test equipment elevation
- ▲E = Elevation Difference (If pipeline has an elevation difference >100' attach pipeline profile dwg)

**Describe How Elevations Determined:** (Line of sight estimation, known data, current survey, information source, ect.)  
 Foot of hydrostatic head was calculated at 9.5' based on 4 psi static head pressure x .433 psi / ft (=9.24') + 6" at bottom of pipe not recorded by the gauge due to location of the gauge itself relative to the center of the pipe.

### TEST PRESSURE CALCULATIONS RESULTS

Nominal Test Pressure: (PSI) 162.375

162.4	psi	Min. Pressure at High Point
166.5	psi	Max. Pressure at Low Point
162.5	psi	Pressure at Test Equipment Point
19.3%		Test Pressure as % SMYS
840.0	psi	100% SMYS
483.8	psi	Design Pressure (Calculated - Pipe Only)

Calculate Max Low Point Pressure:  
(Factor .433 psi / ft for water or Total Ft x .433 (Specific Gravity: 1.0) or correct factor for other test medium);  
 Test Medium: Water  
(Use Formula: p=.433(h)(SG) where p: Pressure / h: Head in Ft / SG: Specific Gravity Test Medium)  
 h: (Ft) 9.5  
 SG: 1

### TEST RESULTS

P <sub>MAX</sub>	=	163.5	psi
P <sub>MIN</sub>	=	163.5	psi
Difference	=		psi

- P<sub>MAX</sub> = Maximum test gauge pressure
- P<sub>MIN</sub> = Minimum test gauge pressure

**Remarks & Assumptions:** We have to assume that the weld joint factor for this pipe is .08 for steel, however no data was available. We also have to assume that the design factor of .72 from ASME is the same because the pipeline is in combustible liquid service.  
 Test pressure determined by max head from a full tank calculated by (.433)(SG)(Height) = 250' high x 1 (SG of water) x .433 = 108.25 x 1.5 = 162.375



PIPELINE PETROLEUM SERVICES, INC.

Pre-Test Calculations & Pressurization Log (Attachment B)

Note: Green cells that are blank indicate a value of 0 (Zero).  
Note: Fill in blue cells with required information / Green cells are calculated values.

Test ID Number:	14-332-01B	Dwg Code Color:	None
Customer:	Willbros Government Services	Date:	6/27/2014
System Under Evaluation:	Tank 5 Fuel Piping - 32"	Location:	Red Hill Fuel Farm

Use this form to establish the pre-test DV/DP, line fill volume, and test pressure volume, as well as plot the actual DV/DP and fill volumes.

Calculated DV / DP Data

DV / DP (Change in Volume / Change in Pressure): DV / DP is defined as the change in volume for an associated change in pressure of a known volume under pressure. Two DV/DP calculations are used in these guidelines, a theoretical and a field value. A theoretical DV/DP will give the expected volume change for an associated change in pressure for the specified volume under test assuming that the volume under pressure is free of entrained gas. The field value of DV/DP is the actual volume change in pressure for the specified volume under test. If air exists within the line under pressure, this value will be different than the theoretical value.

The theoretical DV/DP for aboveground (unrestrained) pipe is calculated through the following equation:

$$\frac{DV}{DP} = V \cdot \left[ \left( \frac{D_o}{E \cdot t} \right) \left( \frac{5}{4} - \nu \right) + C \right]$$

The theoretical DV/DP for buried (restrained) pipe is calculated through the following equation:

$$\frac{DV}{DP} = V \cdot \left[ \left( \frac{D_o}{E \cdot t} \right) (1 - \nu^2) + C \right]$$

where,

- V = volume of the segment for the individual pipe diameter, D (gallons),
- D = outside diameter of pipe (in),
- E = elastic modulus of steel pipe (psi),
- t = wall thickness of pipe (in),
- ν = poisson's ratio of steel pipe,
- C = compressibility of test media (in<sup>3</sup>/in<sup>3</sup>/psi).

NOTE: For a test segment with multiple diameters, sum the individual DV/DP's of each pipe diameter to obtain a total DV/DP for the entire test section.

Restrained Pipe (Underground) (Volume = 0.0408 x d <sup>2</sup> x L)		Unrestrained Pipe (Aboveground & Inside) (Volume = 0.0408 x d <sup>2</sup> x L)	
V <sub>AG</sub>	1753.12	V <sub>AG</sub>	85.20
D <sub>o</sub>	31.25	D <sub>o</sub>	31.25
E	2.95E+07	E	2.95E+07
t	0.375	t	0.375
ν	0.3	ν	0.3
C	3.11E-06	C	3.11E-06
DV/DP <sub>AG</sub>	0.009859816	DV/DP <sub>AG</sub>	0.00493618
Weight of Restrained Pipe	0.92	Weight of Unrestrained Pipe	0.08
AVG DV / DP for Test Section: (Gal)		0.0104524	

Use the Following Information for DV/DP Calculations - Values From Properties Charts Below

Test Medium:	Water
B- Coef of Expansion:	1.23E-04
C-Compressibility of Test Media:	3.11E-06
Pipe Material #1:	Carbon Steel
E = Elastic Modulus of Pipe #1 (PSI):	2.95E+07
ν = Poisson's Ratio of Pipe #1:	0.3
α = Linear Coefficient of Expansion: Pipe #1:	6.10E-06
Pipe Material #2:	N/A
E = Elastic Modulus of Pipe #1 (PSI):	
ν = Poisson's Ratio of Pipe #1:	
α = Linear Coefficient of Expansion: Pipe #2:	
Number of Different Pipe Materials:	1
E Avg For Pipe Materials:	2.95E+07
ν Avg For Pipe Materials:	0.3
α Avg For Pipe Materials:	6.10E-06

Property Chart for Pipe Material

Pipe Material	Elastic Modulus: E	Coefficient of Expansion: α	Linear Coefficient of Expansion: α	Poisson's Ratio: ν
Carbon Steel	2.95E+07	6.50E-06	6.10E-06	.27-.30
Stainless Steel	2.8E+07	9.60E-06		.30-.31
FRP	2.3E+06	1.16E-05	1.16E-05	0.33
Aluminum	1.00E+07			0.33

Property Chart for Test Medium

Test Medium	Compressibility: C = (1/B)	Bulk Modulus: (β)	Coefficient of Expansion: B	SG @ 60°F
JP-8 / JP-8	5.85E-06	1.71E+05	4.98E-04	0.81
Diesel	5.21E-06	1.92E+05	4.59E-04	0.85
Gasoline	5.29E-06	1.89E+05	4.57E-04	0.84
Water	3.11E-06	3.22E+05	1.23E-04	1.00

Test Sections

Pipe Section (Identification)	Pipe Material	Nominal Pipe Ø (in)	Outside Ø (in)	Wall Thickness (in)	AVG Wall Thickness Exposed (AG)	AVG Wall Thickness Buried (BG)	AVG Wall Thickness Inside (IN)	dV/dT: Unrestrained (AG & IN) Pipe, ν(E-3α) Restrained (Buried) Pipes (ν(E-3α)) (Total Last Cell)	Configuration Buried (BG) / Exposed (AG) / Inside (IN)	Length (Ft)	Volume (Gallons)	Volume per Foot Pipe ID	Length AG (% Total Length)(Ft)	Length BG (% Total Length)(Ft)	Length Inside (% Total Length)(Ft)	Volume AG (% Total Length)(Ft)	Volume BG (% Total Length)(Ft)	Volume Inside (% Total Length)(Ft)	
Non Exposed	C87 STD	32	32	0.375		0.375		0.194	Buried	44	1753.12	39.84		44			1753.12		
Nozzle Inside Tank	C87 STD	32	32	0.375			0.375	0.004	Inside	1	39.84	39.84			1				39.84
Nozzle Outside Tank	C87 STD	20	20	0.375			0.375	0.005	Inside	3	45.36	15.12			3				45.36
<b>Total # AG Pipe Sections:</b>						0.375	0.375	0.203		<b>48</b>	<b>1838.32</b>	<b>Totals:</b>		<b>44</b>	<b>4</b>		<b>1753.12</b>	<b>85.20</b>	
<b>Total # BG Pipe Sections:</b>					<b>0.375</b>				Note: AG & IN pipe is calculated as unrestrained.				<b>95.67</b>						<b>19.44</b>
<b>Total # IN Pipe Sections:</b>					<b>0.375</b>				Note: Buried (UG) pipe is calculated as restrained.										
<b>Total # Pipe Sections:</b>					<b>1</b>				Number Exposed Factors:										
<b>Total Exposed Pipe Length: (AG &amp; IN)</b>										<b>4</b> (Ft)									<b>85.20</b> (Gal)
<b>Total Non-Exposed Pipe Length: (UG)</b>										<b>44</b> (Ft)									<b>1753.12</b> (Gal)
																			<b>1.69721</b>







PIPELINE PETROLEUM SERVICES, INC.

Theoretical DV/DP (Test Pressure Fill Chart)(0-453 psi)

Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)
1	0.010452436	51	0.533074177	101	1.05659959	151	1.578317627	201	2.100993967	252	2.634013523	302	3.159639254	352	3.679269884	403	4.21233115
2	0.020904699	52	0.5435266	102	1.06914633	152	1.599770081	202	2.11844227	253	2.644465997	303	3.167087596	354	3.700118153	405	4.232326019
3	0.031357304	53	0.55397933	103	1.07990077	153	1.59922496	203	2.122295691	254	2.654918392	304	3.177540123	355	3.710614208	406	4.243686453
4	0.041809738	54	0.56443147	104	1.0879532	154	1.609574931	204	2.125749306	255	2.665370827	305	3.187662557	356	3.72106723	407	4.254140888
5	0.052262173	55	0.5748839	105	1.09790593	155	1.620127365	205	2.129202921	256	2.675823261	306	3.198444892	357	3.731519157	408	4.264595323
6	0.062714608	56	0.58533634	106	1.10795907	156	1.630680395	206	2.132656536	257	2.686275695	307	3.209597427	358	3.741971582	409	4.275049757
7	0.073167042	57	0.59578877	107	1.11841105	157	1.641232934	207	2.136110151	258	2.69672813	308	3.219346661	359	3.752424027	410	4.285504192
8	0.083619477	58	0.60624121	108	1.12896359	158	1.651785473	208	2.139563766	259	2.707180565	309	3.229802296	360	3.762878461	411	4.295958626
9	0.094071912	59	0.61669364	109	1.13951613	159	1.66233801	209	2.143017391	260	2.717633	310	3.24025673	361	3.773332896	412	4.306413061
10	0.104524346	60	0.62714608	110	1.14976781	160	1.672890534	211	2.205463704	261	2.728085434	311	3.250707165	362	3.78378733	413	4.316867496
11	0.114976781	61	0.63759851	111	1.16022024	161	1.683443163	212	2.215916138	262	2.738537969	312	3.2611596	363	3.79424176	414	4.32732193
12	0.125429215	62	0.64805095	112	1.17067268	162	1.693995692	213	2.22636873	263	2.748990504	313	3.271612034	364	3.8046962	415	4.337776365
13	0.13588165	63	0.65850339	113	1.18112511	163	1.70454821	214	2.236821007	264	2.75944303	314	3.282064469	365	3.815149634	416	4.34823079
14	0.146334085	64	0.66895582	114	1.19157755	164	1.71509977	215	2.247273442	265	2.769895573	315	3.292516904	366	3.825603069	417	4.358685224
15	0.156786519	65	0.67940825	115	1.20203009	165	1.72565131	216	2.257725877	266	2.780348107	316	3.302969338	367	3.836056503	418	4.369139659
16	0.167238954	66	0.68986069	116	1.21248252	166	1.73610384	217	2.268178311	267	2.790800642	317	3.313421773	368	3.846509938	419	4.379594094
17	0.177691388	67	0.70031502	117	1.22293505	167	1.74655637	218	2.278630746	268	2.801253176	318	3.323874207	369	3.856963373	420	4.390048529
18	0.188143823	68	0.71076745	118	1.23338748	168	1.757008905	219	2.289083181	269	2.81170571	319	3.334326642	370	3.867416808	421	4.400502964
19	0.198596258	69	0.72121988	119	1.24384001	169	1.76746143	220	2.299535615	270	2.82215824	320	3.344779077	371	3.877870242	422	4.410957399
20	0.209048692	70	0.73167231	120	1.25429244	170	1.777913964	221	2.30998805	271	2.832610773	321	3.355231511	372	3.888323677	423	4.421411834
21	0.219501127	71	0.74212474	121	1.26474487	171	1.788366493	222	2.320440484	272	2.843063307	322	3.365684046	373	3.898777112	424	4.431866269
22	0.229953562	72	0.75257717	122	1.27519730	172	1.798819022	223	2.330892919	273	2.85351584	323	3.37613648	374	3.909230547	425	4.442320704
23	0.240406006	73	0.76302960	123	1.28564973	173	1.809271551	224	2.341345418	274	2.863968374	324	3.386589015	375	3.919683982	426	4.452775139
24	0.250858441	74	0.77348203	124	1.29610216	174	1.81972408	225	2.351797947	275	2.874420908	325	3.397041415	376	3.930137417	427	4.463229574
25	0.261310876	75	0.78393446	125	1.30655459	175	1.829176609	226	2.362250476	276	2.884873441	326	3.407493846	377	3.940590852	428	4.473684009
26	0.27176331	76	0.79438689	126	1.31700702	176	1.839629138	227	2.372703005	277	2.895325974	327	3.417946277	378	3.951044287	429	4.484138442
27	0.282215745	77	0.80483932	127	1.32745945	177	1.850081667	228	2.383155534	278	2.905778508	328	3.428398708	379	3.961497722	430	4.494592877
28	0.29266818	78	0.81529175	128	1.33791188	178	1.860534196	229	2.393608063	279	2.916231042	329	3.438851139	380	3.971951157	431	4.505047312
29	0.303120614	79	0.82574418	129	1.34836431	179	1.870986725	230	2.404060592	280	2.926683576	330	3.449303564	381	3.982404592	432	4.515501747
30	0.313573049	80	0.83619661	130	1.35881674	180	1.881439254	231	2.414513121	281	2.937136105	331	3.459756091	382	3.992858027	433	4.525956182
31	0.324025484	81	0.84664904	131	1.36926917	181	1.891891783	232	2.42496565	282	2.947588634	332	3.470208522	383	4.003311462	434	4.536410617
32	0.334477919	82	0.85710147	132	1.37972160	182	1.902344312	233	2.435418179	283	2.958041163	333	3.480660951	384	4.013764897	435	4.546865052
33	0.344930354	83	0.86755390	133	1.39017403	183	1.912796841	234	2.445870708	284	2.968493692	334	3.491113381	385	4.024218332	436	4.557319487
34	0.355382789	84	0.87800633	134	1.40062646	184	1.92324937	235	2.456323237	285	2.978946221	335	3.501565811	386	4.034671767	437	4.567773922
35	0.365835224	85	0.88845876	135	1.41107889	185	1.933701904	236	2.466775766	286	2.98939875	336	3.512018241	387	4.045125202	438	4.578228357
36	0.376287659	86	0.89891119	136	1.42153132	186	1.944154233	237	2.477228295	287	2.999851279	337	3.522470671	388	4.055578637	439	4.588682792
37	0.386740094	87	0.90936362	137	1.43198375	187	1.954606762	238	2.487680824	288	3.010303808	338	3.532923101	389	4.066032067	440	4.599137227
38	0.397192529	88	0.91981605	138	1.44243618	188	1.965059291	239	2.498133353	289	3.020756337	339	3.543375531	390	4.076485497	441	4.609591662
39	0.407644964	89	0.93026848	139	1.45288861	189	1.97551182	240	2.508585882	290	3.031208866	340	3.553827961	391	4.086938927	442	4.619546097
40	0.418097399	90	0.94072091	140	1.46334104	190	1.985964351	241	2.519038411	291	3.041661395	341	3.564280391	392	4.097392357	443	4.629500532
41	0.428549834	91	0.95117334	141	1.47379347	191	1.99641682	242	2.52949094	292	3.052113924	342	3.574732821	393	4.107844787	444	4.639954967
42	0.439002269	92	0.96162577	142	1.48424590	192	2.00686939	243	2.539943469	293	3.062566453	343	3.585185251	394	4.118297217	445	4.650409402
43	0.449454704	93	0.97207820	143	1.49469833	193	2.01732192	244	2.550395998	294	3.073018982	344	3.595637681	395	4.128749647	446	4.660863837
44	0.459907139	94	0.98253063	144	1.50515076	194	2.02777439	245	2.560848527	295	3.083471511	345	3.606090111	396	4.139202077	447	4.671318272
45	0.470359574	95	0.99298306	145	1.51560319	195	2.03822686	246	2.571301056	296	3.09392404	346	3.616542541	397	4.149654507	448	4.681772707
46	0.480812009	96	1.00343549	146	1.52605562	196	2.04867933	247	2.581753585	297	3.10437657	347	3.626994971	398	4.160106937	449	4.692227142
47	0.491264444	97	1.01388792	147	1.53650805	197	2.05913180	248	2.592206114	298	3.114829104	348	3.637447401	399	4.170559367	450	4.702681577
48	0.501716879	98	1.02434035	148	1.54706048	198	2.06958427	249	2.602658643	299	3.125281633	349	3.647899831	400	4.181011797	451	4.713136012
49	0.512169314	99	1.03479278	149	1.55751291	199	2.08003674	250	2.613111172	300	3.135734162	350	3.658352261	401	4.191464227	452	4.723590447
50	0.522621749	100	1.04524521	150	1.56796534	200	2.09048921	251	2.623563701	301	3.146186691	351	3.668804691	402	4.201916657	453	4.734044882



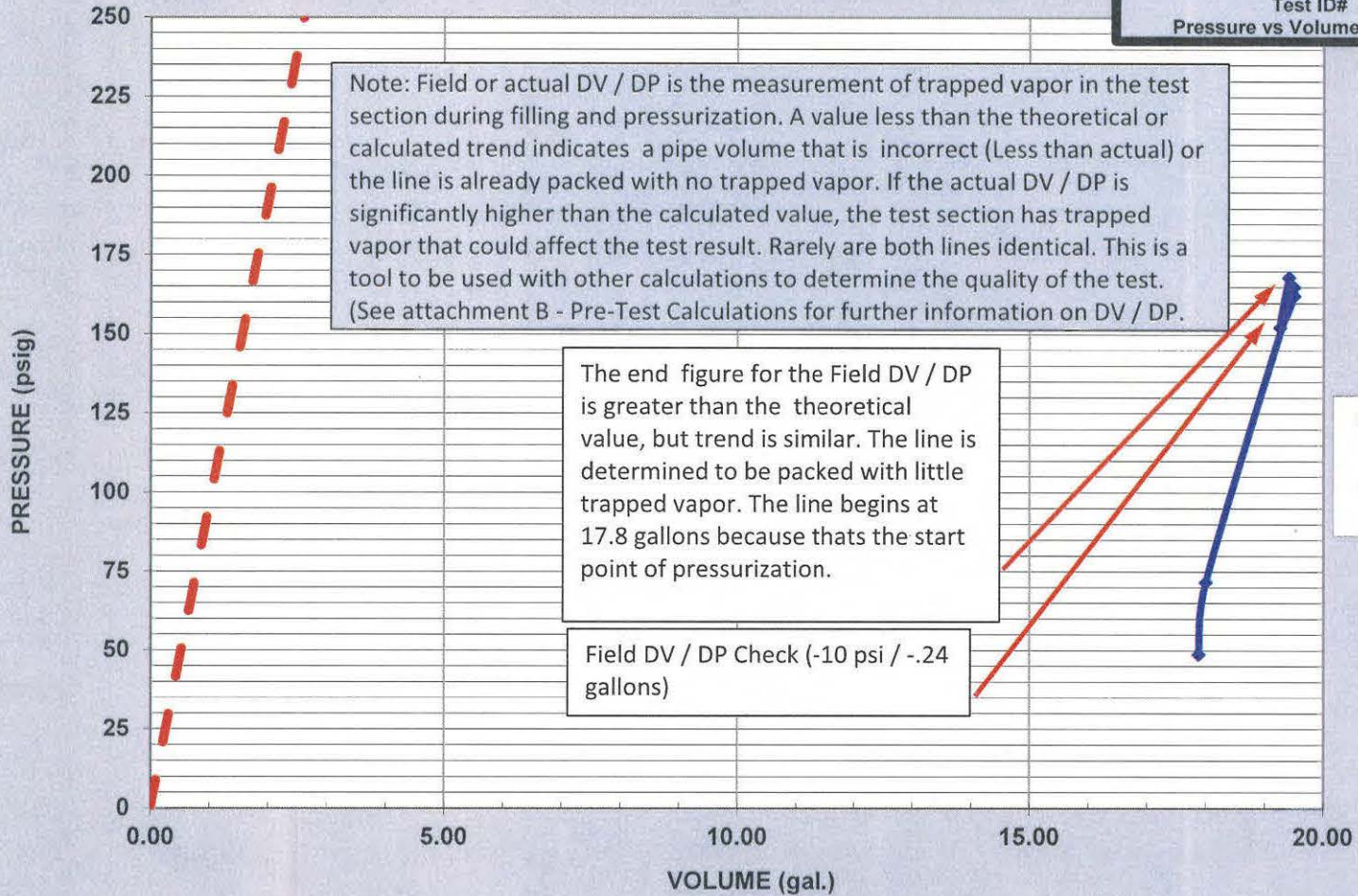
**PIPELINE PETROLEUM SERVICES, INC.**

Red Hill Underground Fuel Facility , HI

Tank 5 - 32" Pipeline - F-76

Test ID# 14-332-01A

Pressure vs Volume Chart / Attachment C







**PIPELINE PETROLEUM SERVICES, INC.**  
**Pipeline Pressure & Temperature Log (Attachment D)**

Date: 6/27/2014  
 Test ID No: 14-332-01B  
 Dwg Color Code: N/A

Note: Enter readings every 15 minutes for first hour of test (Entries 1-5) and every 30 minutes for each hour thereafter.

Customer: Willbros Government Services  
 Location: Red Hill Fuel Farm  
 System: Tank 5 Fuel Piping - 32"

Entry ID Number	Time	Pressure Location		Location 1 & Unit #:		Location 2 & Unit #:		Location 3 & Unit #:		Location 4 & Unit #:		Number AG/IN Sensors:	Number BG Sensors:	Initial Pressurization From:		Remarks (Weather Conditions)			
		Deadweight Pressure (psi)	Chart / Gauge Pressure (psig)	Lower Yard Tunnel (Tank 5)															
1	845	163.5	*	79.34	79.34							1	1			Start Test Time: 845			
2																No weather effects - all piping is not exposed to the elements.			
3																			
4																			
5																			
6																			
7																			
8																			
9																			
10																			
11	930	163.4		79.34	79.34														
12																			
13																			
14																			
15																			
16																			
17																			
18																			
19																			
Final		163.4		79.34	79.34											End Test Time: 930			
Net Change		PSI Diff: -0.1		Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Total Added	Total Drained	Note: Average Temperatures are used in the calculations for the press / temp eval sheet and volume change calculations.			
Average AG/IN Temp Start:				79.34		Average AG/IN Temp End:	79.34	Average Temperature for Test AG/IN:	79.34	Net Volume Loss(+)/ Gain (-):									
Average BG Temp Start:				79.34		Average BG Temp End:	79.34	Average Temperature for Test BG:	79.34										
Equivalent Pressure Loss From Drained Amount: (Field DP / DV)(Hydrotest Only)				PSI Diff + PSI / Gal Equivalent from Drained Product (Calculated) = Total Pressure Differential (TPD)															
1		Gallons =	41.67	PSI		TPD =	-0.10	(Use on Evaluation Sheet - Attachment E)(Hydrotest Only)											
Remarks: (Explanation of Any Pressure Discontinuities)																			
* See attached recorder chart. Average AG Temperature includes both Inside and Aboveground / Exposed Temperatures. (If needed)																			
Used the same temperatures for AG & BG pipe from the dataloggers in the tunnel and inside of the tank because there was no practical way to actually measure the temperature of the piping as it was encased in concrete. Due to the non-exposed nature of all of the piping we feel the temperatures should be very close to each other given the amount of stabilization time allowed.																			
Left pressure on the line from 1200 AM to 0930 Am the next morning and the pressure was at 162.3 psi with a pipe temperature of 79.9.																			





# PIPELINE PETROLEUM SERVICES, INC.

## Hydrostatic Test Pressure and Temperature Evaluation Form (Attachment E)

Test ID Number: 14-332-01B		Dwg Color Code: None		Date: 6/27/14				
Customer: Willbros Government Services			Location: Red Hill Fuel Farm					
System Under Evaluation: Tank 5 Fuel Piping - 32"								
<b>Test Data:</b>								
Test Medium: (Water, Diesel, Gasoline, JP-5, JP-8, Kerosene, Other):		Water		IN: Inside Pipe Temp				
Pipeline Total Length: ("L"): (All Test Sections)		48		AG: Aboveground Pipe Temp				
Pipe Outside Diameter: ("D"): (Average From All Test Sections)		31.250		BG: Below Ground Pipe Temp				
Pipe Wall Thickness: ("t"): (Average From All Test Sections)		0.375		TL: Total Length				
D/t Ratio: (Pipe Ø / "t"): (Average From All Test Sections)		83.33		▲P: Pressure Change				
Pipeline Total Volume: (From Report Page 1)		1838.32		▲T: Temperature Change				
				All temp in degrees Fahrenheit unless noted				
				All pressure in lb/in <sup>2</sup> (psi) unless noted				
Beginning Test Pressure: ("Pb"):		183.5		Ending Test Pressure: ("Pe"):				
				163.4				
Observed Pressure Change (Attachment A): (Change P observed = Pe - Pb):								
				-0.1    ▲ P (PSI)				
Beginning Test Temperature AG: ("Tb AG"):		79.34		Ending Test Temp AG: ("Te AG"):				
				79.34				
Length AG:		Percent Total Length: (Length AG / Total Length):		% TL AG:				
Beginning Test Temperature BG: ("Tb BG"):		79.34		Ending Test Temp BG: ("Te BG"):				
				79.34				
Length BG:		44		Percent Total Length: (Length BG / Total Length):				
				% TL BG:				
				92%				
Beginning Test Temperature Inside: ("Tb IN"):				Ending Test Temp IN: ("Te IN"):				
Length IN:		4		Percent Total Length: (Length IN / Total Length):				
				% TL IN:				
				8%				
▲ T-AG: (Chg T = Te - Tb)		x % TL AG:		= Adjusted Average AG ▲ T:				
▲ T-BG: (Chg T = Te - Tb)		x % TL BG:		= Adjusted Average BG ▲ T:				
▲ T-IN: (Chg T = Te - Tb)		x % TL IN:		= Adjusted Average IN ▲ T:				
(Final (FChg T) = Adjusted Avg AG ▲ T + Adjusted Avg BG ▲ T + Adjusted Avg IN ▲ T / 3)		FChg T:		▲ T (° F)				
Average Temp (T avg)		(Tb AG + Tb BG + Tb IN) / 3 =		Tb    Note: IN & AG are averaged together based on weighting factors.				
		75.66		Te				
				75.66				
Average Fluid / Pipe Temperature (T avg = (Te + Tb) / 2):		T avg:		75.66 (For Test Duration)				
Using T avg and D/t, find dP / dT from temperature compensation charts (exhibit 100,101,102, 103, 104, or 105) or calculate for the appropriate test medium:								
dP / dT =		19.44		psi / ° F    From Pre-Test Calculations - Attachment B				
Formula for dP / dT Chart Development or Calculation used in Attachment B:								
dP = [B-2a] / [Dx(1-v <sup>2</sup> )E(1+C)]		Formula and Results Validated by UFC 3-460-03 Section 9-3.5 / Pressure Relief Valves and CA State Hydrostatic Testing Worksheet. (Different Formula Variation)						
T		C=Compressibility factor for water (Or other test med), cu in/cu in/psig						
dP=psig change per degree C or F		a=Coefficient of expansion for steel,						
B=Coefficient of expansion of test medium		t=Pipe wall thickness, in						
D=Pipe OD in inches		T=Temperature, degrees C or F (20°C)(Or Tavg for test duration above)						
E=Modulus of elasticity for pipe material		Note: Modulus of Elasticity = Young's Modulus = Elastic Modulus						
v=Poisson's ratio, 0.3 for steel pipe								
Test Medium:		Water		Bulk Modulus (β):				
		B=		321,543				
		C= (1/β)		(Reciprocal of the Bulk Modulus (β) in lb/in <sup>2</sup> )				
		1.23E-04						
		3.11E-06						
Pipe Material #1:		Carbon Steel		a =				
		E=		6.50E-06				
Pipe Material #2:		N/A		a =				
		E=						
Pipe Material #3:		N/A		a =				
		E=						
List all Pipe Material & Test Medium Assumptions Made for Test Calculations:    The type and grade of pipe material was assumed because no hard data was available from the original construction of the facility.								
Test Variables for Calculations (Pipe Material Physical Properties from (in part) Appendix C, ASME B 31.3)								
Pipe Material	E	a (in/in/°F)	α (Linear)	Test Medium	C = (1/β)	Bulk Modulus (β):	B (° F)	SG @ 60°F
Carbon Steel	2.95E+07	6.50E-06	6.10E-06	JP-5 / JP-8 / Jet-A / Kerosene	5.18E-06	1.93E+05	4.98E-04	0.81
Stainless Steel	2.8E+07	9.60E-06		Diesel - LSD / ULSD / Dyed	5.21E-06	1.92E+05	4.59E-04	0.85
FRP	2.3E+06	1.16E-05		Gasoline	5.29E-06	1.89E+05	4.57E-04	0.84
Aluminum	1.00E+07			Water	3.11E-06	3.22E+05	1.23E-04	1.00
Other				Other				
Calculate the expected pressure change:    Chg P expected = dP / dT x FChg T								
Figure corrected for various diameters of pipe within test section.								
Chg P expected =		dP / dT		FChg T				
(°C converted to °F)		19.44		(psi / °F) x				
				°F =				
				Chg P				
				psi - Expected    ▲ P				
Pressure increases (Chg P > 0): If Chg P observed > Chg P expected test is successful.								
Pressure decreases (Chg P < 0): If Abs (Chg P observed) < Abs (Chg P expected) test is successful.								
Test Successful: (Pass / Fail):		Fail		Expected ▲ P: (Calculated Chg P)				
				Observed ▲ P: (From Log Sheet)				
				-0.1000				
Note: The sign (+/-) of the observed pressure change should be consistent with the sign of the temperature change (FChg T).								







PIPELINE PETROLEUM SERVICES, INC.

Hydrostatic Test Volume Change Calculations (Attachment C) Page 2 of 2

Test ID Number:	14-332-01B	Code Color:	None
Customer:	Willbros Government Services	Date:	6/27/2014
System Under Evaluation:	Tank 5 Fuel Piping - 32"	Location:	Red Hill Fuel Farm

**Volume Change Calculations for Jet Fuel Pipeline (measured volume/pressure slope method)**

Pipe Data	Test Date	API Gravity																																			
<table border="1"> <tr> <th>Pipe Segment</th> <th>Ø Outside (In)</th> <th>Ø Inside (In)</th> <th>Wall (In)</th> <th>Length (Ft)</th> <th>Volume (Gal)</th> <th>Configuration</th> </tr> <tr> <td>Non Exposed</td> <td>32</td> <td>31.250</td> <td>0.375</td> <td>44</td> <td>1753.12</td> <td>Buried</td> </tr> <tr> <td>Nozzle Inside Tank</td> <td>32</td> <td>31.250</td> <td>0.375</td> <td>1</td> <td>39.84</td> <td>Inside</td> </tr> <tr> <td>Nozzle Outside Tank</td> <td>20</td> <td>19.250</td> <td>0.375</td> <td>3</td> <td>45.96</td> <td>Inside</td> </tr> <tr> <td colspan="4"></td> <td><b>Totals</b></td> <td><b>48</b></td> <td><b>1838.32</b></td> </tr> </table>	Pipe Segment	Ø Outside (In)	Ø Inside (In)	Wall (In)	Length (Ft)	Volume (Gal)	Configuration	Non Exposed	32	31.250	0.375	44	1753.12	Buried	Nozzle Inside Tank	32	31.250	0.375	1	39.84	Inside	Nozzle Outside Tank	20	19.250	0.375	3	45.96	Inside					<b>Totals</b>	<b>48</b>	<b>1838.32</b>	6/27/2014	10
Pipe Segment	Ø Outside (In)	Ø Inside (In)	Wall (In)	Length (Ft)	Volume (Gal)	Configuration																															
Non Exposed	32	31.250	0.375	44	1753.12	Buried																															
Nozzle Inside Tank	32	31.250	0.375	1	39.84	Inside																															
Nozzle Outside Tank	20	19.250	0.375	3	45.96	Inside																															
				<b>Totals</b>	<b>48</b>	<b>1838.32</b>																															

Weighting for segment	% Total Length	Configuration	Buried	Exposed	Inside
Non Exposed	0.95	Buried	0.95		
Nozzle Inside Tank	0.02	Inside			0.02
Nozzle Outside Tank	0.02	Inside			0.02
<b>Sum of Factors</b>		<b>1.00</b>	<b>Weight Factors</b>		
			<b>0.95</b>		<b>0.05</b>

The above factors are used for weighting segment temperatures.

Corrected Temperatures		Initial Test Temperatures		Final Test Temperatures	
Buried	Exposed	Buried	Exposed	Buried	Exposed
79.34	79.34	75.66	79.34	75.66	79.34
		<b>Initial Corrected</b>		<b>Final Corrected</b>	
		75.66		75.66	
		DT1		DT2	
		15.6559661		15.6559661	

**Corrected Temperature Difference**

Initial Pressure	Final Pressure	dPressure	AVG. Pressure
163.5	163.4	-0.1	163.45
			<small>Use Reference from Test Data</small>

**dV/dP Slope Calculations (Values are From Test Data)**

Initial Pressure	Final Pressure	Initial Vol.	Final Vol.	dV/dP
48.7	163.5	17.88	19.41	0.013327526

**Calculating K<sub>T</sub>**

K <sub>T</sub> = 3a - α <sub>90</sub>	K <sub>T</sub>	Coefficient Of Linear Expansion	Temperature Correction Factor
	-0.0003115	a	α <sub>90</sub>
		6.50E-06	3.31E-04

**Calculating Fluid Volume Gain / Loss**

dV = Total Pipeline Volume * K <sub>T</sub> * dT + dV/dP * dP	dV	Net Volume Removed (Accountable Loss(-)/ Gain(+)- From Log Sheet)	Unaccountable Loss	Actual Gain(+)/ Loss(-)
Volume Loss/8hrs	0.00			
Volume Loss/hour	0.00		0.00	
<small>Added or Subtracted During Test</small>				

**CSFM Loss Allowable**

Gal./hour	1.03	Gal./8hours	8.22	Test Conclusion IAW CSFM / hr	Pass
				Test Conclusion IAW CSFM / 8 hrs	Pass

Note: Use this pass/fail criteria to assist in determining a successful test with the temperature evaluation.



**PIPELINE PETROLEUM SERVICES, INC.**

1324 Cavalier Blvd / PO BOX 6808  
Chesapeake, VA 23323  
Phone: (757) 544-0831

**Pipeline Pressure Test Report - Test Summary**

Form Revision Number: 6  
Form Revision Date: 4-Jan-14

Note: Green cells that are blank indicate a value of 0 (Zero).  
Note: Fill in blue cells with required information / Green cells are calculated values.



**I. GENERAL TEST INFORMATION**

Test ID No:	14-332-02	Job No:	14-332	Type of Test:	Hydrostatic Pressure Decay <small>(Hydrostatic x 150% MAWP, Hydraulic x 125% or 150% MAWP) (Hydro-Pneumatic x 110% or 150% MAWP, Pneumatic x 110% MAWP) (Pressure Decay, Strength Test, Leak Test, Spike Test, Etc.)</small>	Minimum Test Duration: (Hrs)	4
Date:	6/25/2014	Customer:	Willbros Government Services			Dwg Color Code:	None
Contract Number:	N/A	System:	Tank 5 Fuel Piping - 18"			Location:	Red Hill Fuel Farm, Naval Station Pearl Harbor
Test Medium:	Water	Tank #:	5	AST / UST:	UST	Product:	Water
Test Medium Source:	Water Line in Lower Access Tunnel	Specific Gravity:	141.5/(131.5 + Degrees API)			API Gravity:	141.5/SG-131.5
Test Medium Additives:	None	Flash Point:	N/A			Flash Point:	N/A
Included Pipe Sections or Laterals: (Test Section)	18" - JP-8 service lateral to Tank 5 from the 12" flange at the wall of the Lower Access Tunnel to the 18" flange inside of the tank where the diverter was connected. (Diverter removed for the test)			Test Connection: (Location / Size / Type)	Ported test blind on the 12" flange located in the lower yard tunnel. Temp probe also placed inside of tank.		
Time Zone:	Hawaii	Country:	USA	Purpose of Test: (Annual Or Five-Year Requalification, New Commissioning, Post Repair, Other)	Possible Suspected Leak		
Test Criteria: (Jurisdictional Regulation)	CSFM / UFC 3-460-03			Skillets Installed:	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No		
Test Procedure:	API RP-1110 / CSFM Guidelines / Willbros Test Procedure, Revision 9: June 5, 2014 <small>(API RP 1110, API 570, ASME B.31.1, ASME B31.3, ASME B31.4, ASME B 31.8, NFPA 329, CSFM, 49 CFR 195)</small>			Location(s): (List valve / tank number / ect)	Size:		
Test Medium Disposal:	<input type="checkbox"/> Yes <input checked="" type="checkbox"/> No			Disposal Company:	N/A		
Disposal Type & Amount (Gals):	N/A			Valves and diffusers removed and test blinds installed.			

**II. PIPE DESIGN DATA**

System Design Data Code: (ASME B 31.1 (Power Piping) / B 31.3 (Process Piping) / B 31.4 (Liquid Fuels Transportation) / B 31.8 (Gas Transmission) / Other)	UNK - Assume ASME B31.3		
Pipe Specification: (ASTM A53 (CS-Welded & Seamless) / A135 (ERW Pipe) / A312 (SS-Welded & Seamless) / API 5L (Welded & Seamless for Fuel Piping) / Other)	UNK - Assume API 5L ERW		
Pipe Grade: (Pipe Grade A & B / Strength X42 - X60)	UNK	SMYS: (psi)	35,000
Year Installed:	Circa 1943		
Known Repairs / Modifications:	Date:	Known Repairs / Modifications:	Date:
None known.			
W <sub>JF</sub> (Weld Joint Factor)	0.8	(Range 1.6 - 1.0 per ASME B 31.4 Table 402.4.3) / Source:	Assumption
D <sub>F</sub> (Design Factor):	0.72	(1/2 for Haz Liquid Pipelines per ASME B31.4 or State Other Criteria):	N/A

**III. TEST SECTIONS (If Loading Arm Present in Test Section include Total Length & Volume from attachment I)**

Pipe Section (Identification)	MP To (Location)	MP From (Location)	Nominal Pipe Ø (in)	Wall Thickness (in)	Outside Ø (in)	Inside Ø (in)	Pipe Material	Configuration (Buried-BG / Exposed-AG / Inside IN)	Length (Ft)	Section as % Total Pipe Length	Volume (Gallons)	Volume per Foot Pipe ID (Gal)	Length AG (%)(Ft)	Length BG (%)(Ft)	Length Inside (%)(Ft)
Non Exposed			18	0.375	18.000	17.25	CS / STD	Buried	58.0	89.23%	704.15	12.14		58.0	
Nozzle Inside Tank			18	0.375	18.000	17.25	CS / STD	Inside	3.0	4.82%	36.42	12.14			3.0
Nozzle Outside Tank			12	0.375	12.750	12	CS / STD	Inside	4.0	6.15%	23.50	5.88			4.0
Total Pipe Sections in Test Section:			3	Averages:	0.375	17.877	15.500	Sum Of Factors:	1.00	Weight Of Factors: (-100%)			0.89	0.11	
Total Volume Test Section (Gal):			764.07	Total Volume Test Section (CF):	102.15	Total Length Test Section: (Ft)	65.0	Total Length AG / BG / Inside: (ft)			58.0	7.0			

Use Factoring For Volume Change & Pressure / Temperature Calculations

Total Number Factors: 2







**Pipeline Pressure Test Report (Continued)**

**VI: ATTACHMENTS TO THIS REPORT: (All May Not Be Included or Required)**

- |   |   |  |
|---|---|--|
| <input checked="" type="checkbox"/> Attachment A / Test Pressure Calculations                 | <input checked="" type="checkbox"/> Attachment F / Volume Change Calculations | <input type="checkbox"/> Pipeline Elevation Drawing    |
| <input checked="" type="checkbox"/> Attachment B / Pre-Test Calculations & Pressurization Log | <input type="checkbox"/> Attachment G / Test Procedure & Valve Line-Up Sheet  | <input type="checkbox"/> Pipeline Test Section Drawing |
| <input checked="" type="checkbox"/> Attachment C / Pressure / Volume Plot                     | <input checked="" type="checkbox"/> Pressure Graph                            | <input type="checkbox"/> Test Equipment Drawing        |
| <input checked="" type="checkbox"/> Attachment D / Pressure & Temp Log                        | <input type="checkbox"/> Attachment H / Loading Arm Information               | <input type="checkbox"/> Disposal Manifest             |
| <input checked="" type="checkbox"/> Attachment E / Pressure & Temperature Evaluation          | <input type="checkbox"/> Attachment I / Photograph Page(s)                    |  |

**VII: GENERAL TEST REMARKS: (List General Pipeline Condition / Recommendations from Visual Inspection)**

Test considered inconclusive IAW applicable jurisdictional regulation, applied industry standards, and the intent of the test.  
 This is not a precision leak detection test and should not be considered as such. This hydrotest is considered a point-in-time, pressure decay, strength / stress / leak test against installed test blinds to determine if there are possible leaks at the stated MAOP / MAWP.  
 Test results are based on criteria established by (in Part) API-RP-1110, California State Fire Marshall Office (CSFM), as well as, calculated thermal pressure loss / gain, calculated volume loss / gain, no visual leaks identified in exposed piping during the test period, good engineering practice, and accepted industry practice. The pass/fail criteria may or may not be the required regulation however the criteria used is the accepted industry practice and is greater than or equal to the requirements in the jurisdictional regulation.

Initial pressurization attempted on the morning of 6/25/14 and the flange gasket inside of the tank began leaking at 162 psi when the stabilization was started. Attempts at tightening flange was unsuccessful. Remove flange and remove defective gasket. Install a new garlok gasket. Re-pressurize to test pressure and flange was tight.

The line pressure never truly stabilized at any time throughout the project.  
 Evidence of the amount of trapped air in the line is the calculated volume to reach test pressure was approximately .57 gallons and it required over 2.5 gallons to reach test pressure.  
 We highly recommend a pneumatic test to confirm the existence of trapped air in the test section.

**VIII: TEST EQUIPMENT INFORMATION:**

(See drawing of testing apparatus if required and Calibration Certificates)

All calibrations are performed third-party and are traceable to NIST.

Equipment Description:	PPSI Unit Number:	Manufacturer:	Serial Number:	Calibration Date:	Calibrated By:
Pipe Pressure Datalogger	Unit 1	MadgeTech	N84154	4/11/2014	Madgetech
4 Channel Temperature Datalogger (Thermocouple)	Unit 1	MadgeTech	N82430	8/21/2013	Madgetech
2 Channel Temperature Datalogger (Thermocouple)	Aux Unit 1	MadgeTech	N84147	8/20/2013	Madgetech
Digital Flowmeter / Totalizer (1/2")	Unit 3	GPI Industries	3206877	6/16/2014	Angels Instruments
Digital Flowmeter / Totalizer (1")	Unit 4	GPI Industries	3710745	6/16/2014	Angels Instruments
0-5000 psi Digital Deadweight Accurate Test Gauge	Unit 1	Crystal	870422	5/5/2014	Angels Instruments

**IX: SIGNATURES**

Tested By: <b>Dennis Cobb</b>	Report Prepared By: <b>Dennis Cobb</b>	Reviewed & Approved: <b>Dennis Cobb</b>	Customer Witness: <b>James Hagen</b>
Title: <b>Vice President</b>	Title: <b>Vice President</b>	Title: <b>Vice President</b>	Title: <b>Project Manager</b>
Signed: 	Signed: 	Signed: 	Company: <b>Willbros Government Services</b>
Date: <b>6/25/2014</b>	Date: <b>6/25/2014</b>	Date: <b>6/25/2014</b>	Signed: (If Required) Date: <b>6/25/2014</b>



# PIPELINE PETROLEUM SERVICES, INC.

## Piping Test Pressure Calculations (Attachment A)

Note: Green cells that are blank indicate a value of 0 (Zero).  
 Note: Fill in blue cells with required information / Green cells are calculated values.

<b>Test ID Number:</b>	14-332-02	<b>Test Section:</b>	Tank 5 Fuel Piping - 18"
<b>Dwg Code Color:</b>	None	<b>Customer:</b>	Willbros Government Services
<b>Date:</b>	6/25/2014	<b>Location:</b>	Red Hill Fuel Farm, Naval Station Pearl Harbor Oahu, HI

### TEST CALCULATIONS INPUT

NPS	=	18.000	in.
D	=	17.677	in.
t	=	0.375	in.
W <sub>JF</sub>	=	0.8	
D <sub>F</sub>	=	0.72	
SMYS	=	35,000	psi
P <sub>WP</sub>	=	108.25	psi
G	=	1	
LE	=		feet
HE	=	9.5	feet
TE	=	9.24	feet
▲E	=	9.5	feet

- NPS= Nominal Pipe Size (Diameter Inches)
- D = Outside Diameter of pipe (in)(Avg of all sections x % total length)
- t = Pipe wall Thickness (in)(Avg of all sections x % total length)
- W<sub>JF</sub> = Weld Joint Factor (From Report Page 1)(Range (.6 - 1.0) per ASME B 31.4 Table 402.4.3)
- D<sub>F</sub> = Design Factor (From Report Page 1)(.72 for Haz Liquid Pipelines per ASME B31.4)
- SMYS = Specified Minimum Yield Strength (From Report Page 1)
- P<sub>WP</sub> = Maximum Working Pressure (psi)
- G = Product (Test Medium) Specific Gravity
- LE = Lowest elevation
- HE = Highest elevation
- TE = Test equipment elevation
- ▲E = Elevation Difference (If pipeline has an elevation difference >100' attach pipeline profile dwg)

**Describe How Elevations Determined:** (Line of sight estimation, known data, current survey, information source, ect.)  
 Foot of hydrostatic head was calculated at 9.5' based on 4 psi static head pressure x .433 psi / ft (=9.24') + 6" at bottom of pipe not recorded by the gauge due to location of the gauge itself relative to the center of the pipe.

### TEST PRESSURE CALCULATIONS RESULTS

Nominal Test Pressure: (PSI) 162.375

162.4	psi	Min. Pressure at High Point
166.5	psi	Max. Pressure at Low Point
162.5	psi	Pressure at Test Equipment Point
10.9%		Test Pressure as % SMYS
1485.0	psi	100% SMYS
855.4	psi	Design Pressure (Calculated - Pipe Only)

**Calculate Max Low Point Pressure:**  
 (Factor .433 psi / ft for water or Total Ft x .433 (Specific Gravity: 1.0) or correct factor for other test medium):

Test Medium: Water

(Use Formula: p=.433(h)(SG) where p: Pressure / h: Head in Ft / SG: Specific Gravity Test Medium)

h: (Ft) 9.5

SG: 1

### TEST RESULTS

P <sub>MAX</sub>	=	165.2	psi
P <sub>MIN</sub>	=	165.2	psi
Difference	=		psi

- P<sub>MAX</sub> = Maximum test gauge pressure
- P<sub>MIN</sub> = Minimum test gauge pressure

**Remarks & Assumptions:** We have to assume that the weld joint factor for this pipe is .08 for steel, however no data was available. We also have to assume that the design factor of .72 from ASME is the same because the line is in combustible liquid service.  
 Test pressure determined by max head from a full tank calculated by (.433)(SG)(Height) = 250' high x 1 (SG of water) x .433 = 108.25 x 1.5 = 162.375



PIPELINE PETROLEUM SERVICES, INC.

Pre-Test Calculations & Pressurization Log (Attachment B)

Note: Green cells that are blank indicate a value of 0 (Zero).  
 Note: Fill in blue cells with required information / Green cells are calculated values.

Test ID Number:	14-332-02	Dwg Code Color:	None
Customer:	Willbros Government Services	Date:	6/25/2014
System Under Evaluation:	Tank 5 Fuel Piping - 18"	Location:	Red Hill Fuel Farm, Naval Station Pearl Harbor

Use this form to establish the pre-test DV/DP, line fill volume, and test pressure volume, as well as plot the actual DV/DP and fill volumes.

Calculated DV / DP Data  
 DV / DP (Change in Volume / Change in Pressure): DV / DP is defined as the change in volume under pressure of a known volume under pressure. Two DV/DP calculations are used in these guidelines, a theoretical and a field value. A theoretical DV/DP will give the expected volume change for an associated change in pressure for the specified volume under test assuming that the volume under pressure is free of entrained gas. The field value of DV/DP is the actual volume change for an associated change in pressure for the specified volume under test. If air exists within the line under pressure, this value will be different than the theoretical value.

The theoretical DV/DP for aboveground (unrestrained) pipe is calculated through the following equation:

$$\frac{DV}{DP} = V \cdot \left[ \left( \frac{D}{E \cdot t} \right) \left( \frac{5}{4} - \nu \right) + C \right]$$

The theoretical DV/DP for buried (restrained) pipe is calculated through the following equation:

$$\frac{DV}{DP} = V \cdot \left[ \left( \frac{D}{E \cdot t} \right) (1 - \nu^2) + C \right]$$

where,

V = volume of the segment for the individual pipe diameter, D (gallons)  
 D = outside diameter of pipe (in)  
 E = elastic modulus of steel pipe (psi)  
 t = wall thickness of pipe (in)  
 ν = poisson's ratio of steel pipe  
 C = compressibility of test media (in<sup>3</sup>/in<sup>3</sup>/psi).

NOTE: For a test segment with multiple diameters, sum the individual DV/DP's of each pipe diameter to obtain a total DV/DP for the entire test section.

Restrained Pipe (Underground) (Volume = 0.0408 x d <sup>2</sup> x L)		Unrestrained Pipe (Aboveground & Inside) (Volume = 0.0408 x d <sup>2</sup> x L)	
From Formula at Left (CSFM)		From Formula at Left (CSFM)	
√s	704.15	√s	59.92
D	17.67692308	D	17.67692308
E	2.95E+07	E	2.95E+07
t	0.375	t	0.375
ν	0.3	ν	0.3
C	3.11E-06	C	3.11E-06
DV/DP <sub>th</sub>	0.003213813	DV/DP <sub>th</sub>	0.00027322
Weight of Restrained Pipe:	0.89	Weight of Unrestrained Pipe:	0.11
AVG DV / DP for Test Section: (Gal)		0.0034911	

Use the Following Information for DV / DP Calculations - Values From Properties Charts Below

Test Medium:	Water		
B= Coef of Expansion:	1.23E-04	C=Compressibility of Test Media:	3.11E-06
Pipe Material #1:	Carbon Steel		
E = Elastic Modulus of Pipe #1 (PSI): 2.95E+07			
ν = Poisson's Ratio of Pipe #1: 0.3			
α = Linear Coefficient of Expansion: Pipe #1: 6.10E-06			
Pipe Material #2:	N/A		
E = Elastic Modulus of Pipe #1 (PSI):			
ν = Poisson's Ratio of Pipe #1:			
α = Linear Coefficient of Expansion: Pipe #2:			
Number of Different Pipe Materials: 1			
E Avg For Pipe Materials: 2.95E+07			
ν Avg For Pipe Materials: 0.3			
α Avg For Pipe Materials: 6.10E-06			

Property Chart for Pipe Material

Pipe Material	Elastic Modulus: E	Coefficient of Expansion: α	Linear Coefficient of Expansion: α	Poisson's Ratio: ν
Carbon Steel	2.95E+07	6.50E-06	6.10E-06	.27-.30
Stainless Steel	2.8E+07	9.60E-06		.30-.31
FRP	2.3E+06	1.16E-05	1.16E-05	0.33
Aluminum	1.00E+07			0.33

Property Chart for Test Medium

Test Medium	Compressibility: C = (1/β)	Bulk Modulus: (β)	Coefficient of Expansion: B	SG @ 60°F
JP-5 / JP-8	5.85E-06	1.71E+05	4.98E-04	0.81
Diesel	5.21E-06	1.92E+05	4.98E-04	0.85
Gasoline	5.29E-06	1.89E+05	4.57E-04	0.84
Water	3.11E-06	3.22E+05	1.23E-04	1.00

Test Sections

Pipe Section (Identification)	Pipe Material	Nominal Pipe Ø (in)	Outside Ø (in)	Wall Thickness (in)	AVG Wall Thickness Exposed (AG)	AVG Wall Thickness Buried (BG)	AVG Wall Thickness Inside (IN)	dV/dT: Unrestrained (AG & IN) Pipe: (V(B-2α) / (Total Last Cell))	Configuration Buried-BG / Exposed-AG / Inside-IN	Length (Ft)	Volume (Gallons)	Volume per Foot Pipe ID	Length AG (% Total Length)(Ft)	Length BG (% Total Length)(Ft)	Length Inside (% Total Length)(Ft)	Volume AG (% Total Length)(Ft)	Volume BG (% Total Length)(Ft)	Volume Inside (% Total Length)(Ft)	
Non Exposed	CS / STD	18	18	0.375		0.375		0.078	Buried	58	704.15	12.14		58			704.15		
Nozzle Inside Tank	CS / STD	18	18	0.375		0.375		0.004	Inside	3	36.42	12.14			3				36.42
Nozzle Outside Tank	CS / STD	12	12.75	0.375		0.375		0.002	Inside	4	23.50	5.88			4				23.50
Total # AG Pipe Sections:						0.375	0.375	0.084	Total Length:	65	764.07	Totals:					704.15		59.92
Total # BG Pipe Sections:					1	AVG Wall AG & IN:	0.375	Note: AG & IN pipe is calculated as unrestrained.	dP/dV (=1/DV/DP) (dV/dP calculated above)(psi/gal) =		286.44	dP/dT: (=dP/dV)x(dV/dT)psi/°F =		24.15					
Total # IN Pipe Sections:					2	AVG Wall Buried:	0.375	Note: Buried (UG) pipe is calculated as restrained.	dP/dV: Change in pressure with respect to volume.		0.084	dV/dT: Change in volume with respect to temperature							
Total # Pipe Sections:					3	Number Exposed Factors:	1		dV/dT: Change in volume with respect to temperature										
Total Exposed Pipe Length: (AG & IN)					7	(Ft)	Total Exposed Volume: (AG & IN)	59.92	(Gal)	Total Volume to Fill Test Section (If Line Empty)(Gal):	764.07								
Total Non-Exposed Pipe Length: (UG)					58	(Ft)	Total Non-Exposed Volume: (UG)	704.15	(Gal)	Test Pressure (From Report Page 1)(PSI):	162.575								
										Total Volume to Reach Test Pressure From 0 psi (Use DV / DP Chart Below)(Gal):	9.86687								







PIPELINE PETROLEUM SERVICES, INC.

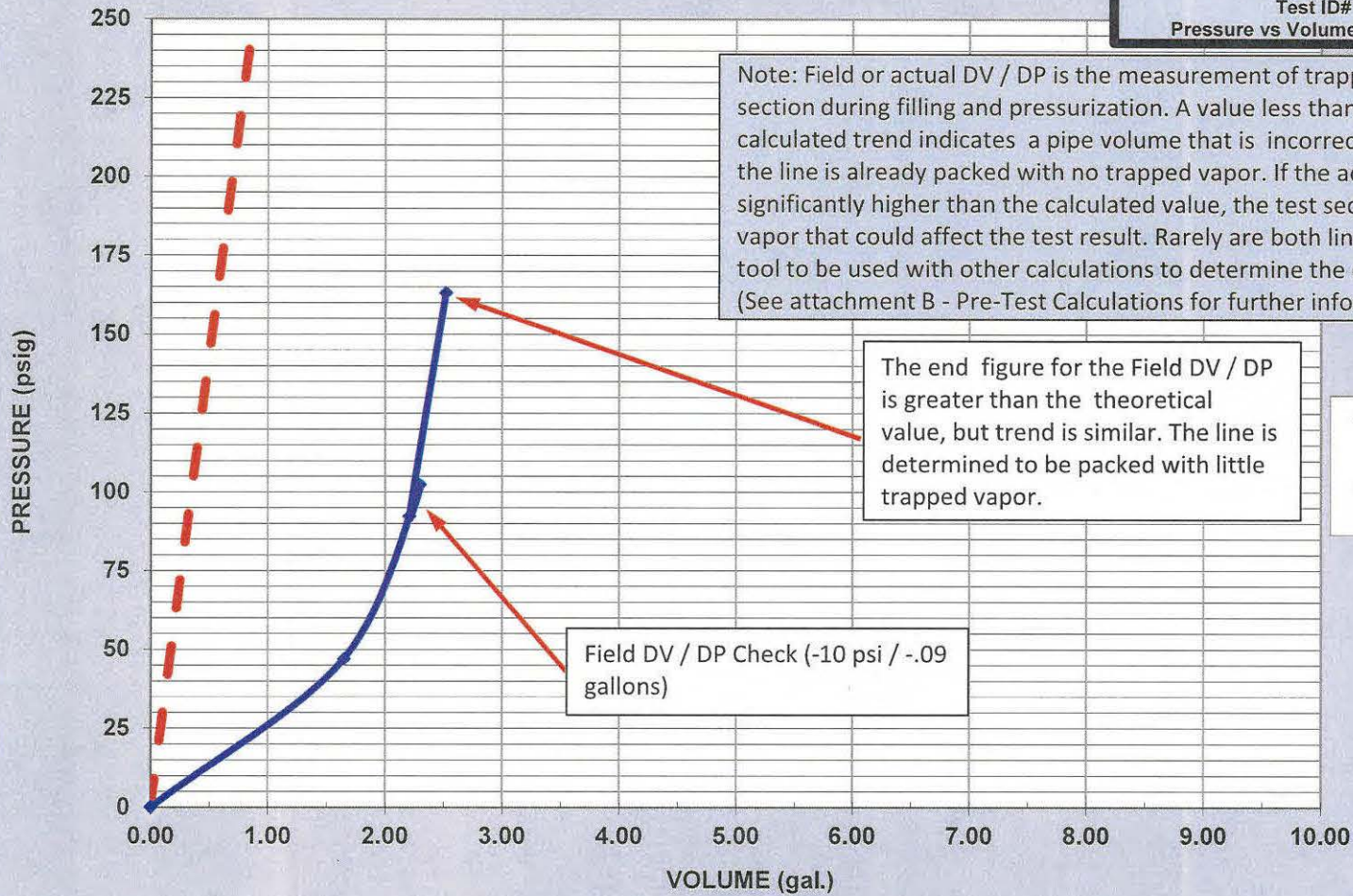
Theoretical DV/DP (Test Pressure Fill Chart)(0-453 psi)

Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)	Pressure (PSI)	Volume (Gallons)
1	0.003491135	51	0.17604798	101	0.35269493	151	0.527181371	201	0.701718177	252	0.876254987	302	1.050792742	352	1.225326498	403	1.40087237
2	0.00698227	52	0.18153902	102	0.35929576	152	0.530652506	203	0.708700396	253	0.883257132	303	1.054322742	353	1.229370623	404	1.4104185
3	0.010473405	53	0.18503015	103	0.3599869	153	0.534143641	204	0.71181521	254	0.886748262	304	1.061305012	355	1.239352893	406	1.41740077
4	0.01396454	54	0.18852129	104	0.36307803	154	0.537634776	205	0.715882696	255	0.890239402	305	1.064796147	356	1.242844028	407	1.42089191
5	0.017455676	55	0.19201242	105	0.36656917	155	0.541125911	206	0.719173791	256	0.893730537	306	1.068287282	357	1.246335162	408	1.42438304
6	0.020946808	56	0.19550355	106	0.3700603	156	0.544617046	207	0.722664926	257	0.897221672	307	1.071778417	358	1.249826297	409	1.42787418
7	0.024437944	57	0.19899469	107	0.37355144	157	0.548108181	208	0.726156061	258	0.900712806	308	1.075269552	359	1.253317432	410	1.43136531
8	0.027929079	58	0.20248582	108	0.37704257	158	0.551599316	209	0.729647196	259	0.904203941	309	1.078760687	360	1.256808587	411	1.43485645
9	0.031420214	59	0.20597696	109	0.38053371	159	0.555090451	210	0.733138331	260	0.907695076	310	1.082251822	361	1.260299722	412	1.43834758
10	0.034911349	60	0.20946809	110	0.38402484	160	0.558581585	211	0.736629466	261	0.911186211	311	1.085742957	362	1.263790857	413	1.44183872
11	0.038402484	61	0.21295923	111	0.38751597	161	0.56207272	212	0.740120601	262	0.914677346	312	1.089234092	363	1.267281992	414	1.44532985
12	0.041893619	62	0.21645036	112	0.39100711	162	0.565563855	213	0.743611736	263	0.918168481	313	1.092725227	364	1.270773127	415	1.44882099
13	0.045384754	63	0.2199415	113	0.39449824	163	0.56905499	214	0.74710287	264	0.921659616	314	1.096216361	365	1.274264262	416	1.45231212
14	0.048875889	64	0.22343263	114	0.39798938	164	0.572546125	215	0.750594025	265	0.925150751	315	1.099707496	366	1.277755397	417	1.45580325
15	0.052367024	65	0.22692377	115	0.40148051	165	0.57603725	216	0.75408515	266	0.928641886	316	1.103198631	367	1.281246532	418	1.45929439
16	0.055858159	66	0.2304149	116	0.40497165	166	0.57952838	217	0.75757628	267	0.932133021	317	1.106689766	368	1.284737667	419	1.46278553
17	0.059349294	67	0.23390604	117	0.40846278	167	0.58301953	218	0.76106741	268	0.935624156	318	1.110180901	369	1.288228802	420	1.46627666
18	0.062840429	68	0.23739717	118	0.41195392	168	0.586510665	219	0.764558545	269	0.93911529	319	1.113672036	370	1.291719937	421	1.4697678
19	0.066331564	69	0.24088831	119	0.41544505	169	0.5900018	220	0.76804968	270	0.942606425	320	1.117163171	371	1.295211071	422	1.47325893
20	0.069822699	70	0.24437944	120	0.41893619	170	0.593492935	221	0.771540815	271	0.94609756	321	1.120654306	372	1.298702206	423	1.47675007
21	0.073313833	71	0.24787058	121	0.42242732	171	0.596984069	222	0.77503195	272	0.949588695	322	1.124145441	373	1.302193341	424	1.4802412
22	0.076804968	72	0.25136171	122	0.42591846	172	0.600475204	223	0.778523085	273	0.95307983	323	1.127636576	374	1.305684476	425	1.48373234
23	0.080296103	73	0.25485285	123	0.42940959	173	0.603966338	224	0.78201422	274	0.956570965	324	1.13112771	375	1.309175611	426	1.48722347
24	0.083787238	74	0.25834398	124	0.43290073	174	0.607457474	225	0.78550536	275	0.9600621	325	1.134618845	376	1.312666745	427	1.49071461
25	0.087278373	75	0.26183512	125	0.43639186	175	0.610948609	226	0.788996498	276	0.963553235	326	1.13810998	377	1.31615788	428	1.49420574
26	0.090769508	76	0.26532625	126	0.439883	176	0.614439744	227	0.792487634	277	0.96704437	327	1.141601115	378	1.319649015	429	1.49769688
27	0.094260643	77	0.26881739	127	0.44337413	177	0.617930879	228	0.795978769	278	0.970535505	328	1.14509225	379	1.32314015	430	1.50118801
28	0.097751777	78	0.27230852	128	0.44686527	178	0.621422014	229	0.799469914	279	0.97402664	329	1.148583385	380	1.326631285	431	1.50467915
29	0.101242912	79	0.27580065	129	0.4503564	179	0.624913149	230	0.802961049	280	0.977517774	330	1.15207452	381	1.33012242	432	1.50817028
30	0.104734047	80	0.27929279	130	0.45384754	180	0.628404284	231	0.806452184	281	0.981008909	331	1.155565655	382	1.333613555	433	1.51166142
31	0.108225182	81	0.28278393	131	0.45733867	181	0.631895418	232	0.809943319	282	0.984500044	332	1.15905679	383	1.33710467	434	1.51515255
32	0.111716317	82	0.28627506	132	0.46082981	182	0.635386553	233	0.813434453	283	0.987991179	333	1.162547925	384	1.340595805	435	1.51864369
33	0.115207452	83	0.2897662	133	0.46432094	183	0.638877688	234	0.816925588	284	0.991482314	334	1.16603906	385	1.34408694	436	1.52213482
34	0.118698587	84	0.29325733	134	0.46781208	184	0.642368823	235	0.820416723	285	0.994973449	335	1.169530194	386	1.347578074	437	1.52562596
35	0.122189722	85	0.29674847	135	0.47130321	185	0.645859958	236	0.823907858	286	0.998464584	336	1.173021329	387	1.35106921	438	1.52911709
36	0.125680857	86	0.3002396	136	0.47479435	186	0.649351093	237	0.827398993	287	1.001955719	337	1.176512464	388	1.354560345	439	1.53260822
37	0.129171992	87	0.30373074	137	0.47828548	187	0.652842228	238	0.830890128	288	1.005446854	338	1.180003599	389	1.35805148	440	1.53609935
38	0.132663127	88	0.30722188	138	0.48177662	188	0.656333363	239	0.834381263	289	1.008937989	339	1.183494734	390	1.361542614	441	1.53959049
39	0.136154262	89	0.31071301	139	0.48526775	189	0.659824498	240	0.837872398	290	1.012429124	340	1.186985869	391	1.365033749	442	1.54308163
40	0.139645397	90	0.31420414	140	0.48875889	190	0.663315633	241	0.841363533	291	1.015920259	341	1.190477004	392	1.368524884	443	1.54657276
41	0.143136532	91	0.31769528	141	0.49225002	191	0.666806768	242	0.844854668	292	1.019411393	342	1.193968139	393	1.372016019	444	1.5500639
42	0.146627667	92	0.32118641	142	0.49574116	192	0.670297902	243	0.848345802	293	1.022902528	343	1.197459274	394	1.375507154	445	1.55355503
43	0.150118802	93	0.32467755	143	0.49923229	193	0.673789037	244	0.851836937	294	1.026393663	344	1.200950409	395	1.378998289	446	1.55704617
44	0.153609937	94	0.32816868	144	0.50272343	194	0.677280172	245	0.855328072	295	1.029884802	345	1.204441544	396	1.382489424	447	1.5605373
45	0.157101072	95	0.33165982	145	0.50621456	195	0.680771307	246	0.858819207	296	1.033375937	346	1.207932679	397	1.385980559	448	1.56402844
46	0.160592207	96	0.33515095	146	0.5097057	196	0.684262442	247	0.862310342	297	1.036867072	347	1.211423813	398	1.389471694	449	1.56751957
47	0.164083342	97	0.33864209	147	0.51319683	197	0.687753577	248	0.865801477	298	1.040358207	348	1.214914948	399	1.392962829	450	1.57101071
48	0.167574477	98	0.34213322	148	0.51668797	198	0.691244712	249	0.869292612	299	1.043849342	349	1.218406083	400	1.396453964	451	1.57450184
49	0.171065612	99	0.34562436	149	0.5201351	199	0.694735847	250	0.872783747	300	1.047340477	350	1.221897217	401	1.399945099	452	1.57799297
50	0.174556747	100	0.34912549	150	0.52362624	200	0.698226982	251	0.876274882	301	1.050831612	351	1.225388352	402	1.403436233	453	1.58148411



**PIPELINE PETROLEUM SERVICES, INC.**

Red Hill Underground Fuel Facility, HI  
Tank 5- 18" Line - JP-8  
Test ID# 14-332-02  
Pressure vs Volume Chart / Attachment C



Note: Field or actual DV / DP is the measurement of trapped vapor in the test section during filling and pressurization. A value less than the theoretical or calculated trend indicates a pipe volume that is incorrect (Less than actual) or the line is already packed with no trapped vapor. If the actual DV / DP is significantly higher than the calculated value, the test section has trapped vapor that could affect the test result. Rarely are both lines identical. This is a tool to be used with other calculations to determine the quality of the test. (See attachment B - Pre-Test Calculations for further information on DV / DP.

The end figure for the Field DV / DP is greater than the theoretical value, but trend is similar. The line is determined to be packed with little trapped vapor.

Field DV / DP Check (-10 psi / -.09 gallons)

- Theoretical DV/DP
- Actual DV/DP





**PIPELINE PETROLEUM SERVICES, INC.**  
**Pipeline Pressure & Temperature Log (Attachment D)**

Date: 6/25/2014  
 Test ID No: 14-332-02  
 Dwg Color Code: N/A

Note: Enter readings every 15 minutes for first hour of test (Entries 1-5) and every 30 minutes for each hour thereafter.

Customer: Willbros Government Services  
 Location: Red Hill Fuel Farm, Naval Station Pearl Harbor  
 System: Tank 5 Fuel Piping - 18"

Entry ID Number	Time	Pressure Location		Location 1 & Unit #:	Location 2 & Unit #:	Location 3 & Unit #:	Location 4 & Unit #:	Number AG/IN Sensors:	Number BG Sensors:	Initial Pressurization From:		PSI	Remarks (Weather Conditions)			
		Deadweight Pressure (ps)	Chart / Gauge Pressure (psig)	Lower Yard Tunnel (Tank 5)	Lower Yard Tunnel (Tank 5)			1	1							
		Aboveground / Exposed Pipe Temp (F) Location 1	Belowground / Non-Exposed Pipe Temp (F) Location 1	Aboveground / Exposed Pipe Temp (F) Location 2	Belowground / Non-Exposed Pipe Temp (F) Location 2	Aboveground / Exposed Pipe Temp (F) Location 3	Belowground / Non-Exposed Pipe Temp (F) Location 3	Aboveground / Exposed Pipe Temp (F) Location 4	Belowground / Non-Exposed Pipe Temp (F) Location 4	Inside Pipe Temp (F)	Ambient Temp (F)	Volume Added (Gal)	Volume Drained (Gal)	Percent Cloud Cover (0-100%)		
1	2237	165.2		79.84	79.84						79.81				Start Test	Time: 2237
2																
3																
4																
5																
6																
7																
8																
9																
10																
11	0137	162.0		79.75	79.75						79.68					
12																
13																
14																
15																
16																
17																
18																
19																
Final		162.0		79.75	79.75						79.68				End Test	Time: 0137
Net Change		PSI Diff		Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Temp Diff	Total Added	Total Drained	Note: Average Temperatures are used in the calculations for the press / temp eval sheet and volume change calculations.		
		-3.2		-0.09	-0.09											
Average AG/IN Temp Start:				79.84		Average AG/IN Temp End:				79.75		Average Temperature for Test AG/IN:		79.80		Net Volume Loss(+) / Gain (-):
Average BG Temp Start:				79.84		Average BG Temp End:				79.75		Average Temperature for Test BG:		79.80		
Equivalent Pressure Loss From Drained Amount: (Field DP / DV)(Hydrotest Only)						PSI Diff + PSI / Gal Equivalent from Drained Product (Calculated) = Total Pressure Differential (TPD)										
1		Gallons =		111.11		PSI		TPD =		-3.20		(Use on Evaluation Sheet - Attachment E)(Hydrotest Only)				
		Total Gal Drained =				PSI										
<b>Remarks: (Explanation of Any Pressure Discontinuities)</b>																
* See attached recorder chart. Average AG Temperature includes both Inside and Aboveground / Exposed Temperatures. (If needed)																
Used the same temperatures for AG & BG pipe from the dataloggers in the tunnel and inside of the tank because there was no practical way to actually measure the temperature of the piping as it was encased in concrete. Due to the non-exposed nature of all of the piping we feel the temperatures should be very close to each other given the amount of stabilization time allowed.																
Left pressure on the line from 1600 on June 25 (Pressure: 167.65 / Pipe Temp: 80.024 + 79.466) to 0915 AM the next morning and the pressure was at 154.7 psi with a pipe temperature of 79.826 + 79.61.																
Note: Line never fully stabilized.																





# PIPELINE PETROLEUM SERVICES, INC.

## Hydrostatic Test Pressure and Temperature Evaluation Form (Attachment E)

Test ID Number:	14-332-02	Dwg Color Code:	None	Date:	6/25/14			
Customer:	Willbros Government Services		Location:	Red Hill Fuel Farm, Naval Station Pearl Harbor				
System Under Evaluation:	Tank 5 Fuel Piping - 18"							
<b>Test Data:</b>			IN: Inside Pipe Temp					
Test Medium: (Water, Diesel, Gasoline, JP-5, JP-8, Kerosene, Other):	Water		AG: Aboveground Pipe Temp					
Pipeline Total Length: ("L"): (All Test Sections)	65		BG: Below Ground Pipe Temp					
Pipe Outside Diameter: ("D"): (Average From All Test Sections)	17.677		TL: Total Length					
Pipe Wall Thickness: ("t"): (Average From All Test Sections)	0.375		ΔP: Pressure Change					
D/t Ratio: (Pipe Ø / "t"): (Average From All Test Sections)	47.14		ΔT: Temperature Change					
Pipeline Total Volume: (From Report Page 1)	764.07		All temp in degrees Fahrenheit unless noted					
Beginning Test Pressure: ("Pb"):	165.2		Ending Test Pressure: ("Pe"):	162				
Observed Pressure Change (Attachment A): (Change P observed = Pe - Pb):			-3.2	ΔP (PSI)				
Beginning Test Temperature AG: ("Tb AG"):	79.84		Ending Test Temp AG: ("Te AG"):	79.75				
Length AG:			Percent Total Length: (Length AG / Total Length): % TL AG:					
Beginning Test Temperature BG: ("Tb BG"):	79.84		Ending Test Temp BG: ("Te BG"):	79.75				
Length BG:	58		Percent Total Length: (Length BG / Total Length): % TL BG:	89%				
Beginning Test Temperature Inside: ("Tb IN"):			Ending Test Temp IN: ("Te IN"):					
Length IN:	7		Percent Total Length: (Length IN / Total Length): % TL IN:	11%				
ΔT-AG: (Chg T=Te -Tb)	-0.09		x %TL AG:	= Adjusted Average AG ΔT:				
ΔT-BG: (Chg T=Te -Tb)	-0.09		x %TL BG:	= Adjusted Average BG ΔT:				
ΔT-IN: (Chg T=Te -Tb)			x %TL IN:	= Adjusted Average IN ΔT:				
(Final (FChg T) = Adjusted Avg AG ΔT + Adjusted Avg BG ΔT + Adjusted Avg IN ΔT / 3)			FChg T:	-0.07				
Average Temp (T avg)	(Tb AG + Tb BG + Tb IN) / 3 = 73.58		Tb	Note: IN & AG are averaged together based on weighting factors.				
	(Te AG + Te BG + Te IN) / 3 = 73.50		Te					
Average Fluid / Pipe Temperature (T avg = (Te + Tb) / 2):			T avg:	73.54 (For Test Duration)				
Using T avg and D/t, find dP / dT from temperature compensation charts (exhibit 100,101,102, 103, 104, or 105) or calculate for the appropriate test medium:								
dP / dT =	24.15		psi / °F From Pre-Test Calculations - Attachment B					
Formula for dP / dT Chart Development or Calculation used in Attachment B:								
dP = [B-2aV] / [Dx(1-v <sup>2</sup> )E(1+C)]		Formula and Results Validated by UFC 3-460-03 Section 9-3.5 / Pressure Relief Valves and CA State Hydrostatic Testing Worksheet. (Different Formula Variation)						
T		C=Compressibility factor for water (Or other test med), cu in/cu in/psig						
dP=psig change per degree C or F		a=Coefficient of expansion for steel,						
B=Coefficient of expansion of test medium		t=Pipe wall thickness, in						
D=Pipe OD in inches		T=Temperature, degrees C or F (20°C)(Or Tavg for test duration above)						
E=Modulus of elasticity for pipe material		v=Poisson's ratio, 0.3 for steel pipe						
v=Poisson's ratio, 0.3 for steel pipe		Note: Modulus of Elasticity = Young's Modulus = Elastic Modulus						
Test Medium:	Water	B=	1.23E-04	Bulk Modulus (β):	321,543			
		C = (1/β)	3.11E-06	(Reciprocal of the Bulk Modulus (β) in lb/in <sup>2</sup> )				
Pipe Material #1:	Carbon Steel	E=	2.95E+07	a =	6.50E-06			
Pipe Material #2:	N/A	E=		a =				
Pipe Material #3:	N/A	E=		a =				
List all Pipe Material & Test Medium Assumptions Made for Test Calculations:								
Test Variables for Calculations (Pipe Material Physical Properties from (in part) Appendix C, ASME B 31.3)								
Pipe Material	E	a (in/in/°F)	α (Linear)	Test Medium	C = (1/β)	Bulk Modulus (β):	B (°F)	SG @ 60°F
Carbon Steel	2.95E+07	6.50E-06	6.10E-06	JP-5 / JP-8 / Jet-A / Kerosene	5.18E-06	1.93E+05	4.98E-04	0.81
Stainless Steel	2.8E+07	9.60E-06		Diesel - LSD / ULSD / Dyed	5.21E-06	1.92E+05	4.59E-04	0.85
FRP	2.3E+06	1.16E-05		Gasoline	5.29E-06	1.89E+05	4.57E-04	0.84
Aluminum	1.00E+07			Water	3.11E-06	3.22E+05	1.23E-04	1.00
Other				Other				
Calculate the expected pressure change: Chg P expected = dP / dT x FChg T								
Figure corrected for various diameters of pipe within test section.								
Chg P expected =	dP / dT	FChg T	Chg P					
(°C converted to °F)	24.15	(psi / °F) x -0.07	°F = -1.73	psi - Expected ΔP				
Pressure increases (Chg P > 0): If Chg P observed > Chg P expected test is successful.								
Pressure decreases (Chg P < 0): If Abs (Chg P observed) < Abs (Chg P expected) test is successful.								
Test Successful: (Pass / Fail):	Fail		Expected Δ P: (Calculated Chg P)	-1.7302				
Total pressure differential (TPD) from Attachment A (Log Sheet) →			Observed Δ P: (From Log Sheet)	-3.2000				
Note: The sign (+/-) of the observed pressure change should be consistent with the sign of the temperature change (FChg T).								



PIPELINE PETROLEUM SERVICES, INC.

Hydrostatic Test Volume Change Calculations (Attachment F) Page 1 of 2							
Test ID Number:	14-332-02			Dwg Code Color:	None		
Customer:	Willbros Government Services			Date:	6/25/2014		
System Under Evaluation:	Tank 5 Fuel Piping - 18"			Location:	Red Hill Fuel Farm, Naval Station Pearl Harbor		
Volume Change Calculations for Pipeline Hydrostatic Test (Calculated Volume/Pressure Slope Method)							
Standard Formula:	$\Delta V / V = K_p \Delta P + K_I \Delta T$			Where:	$K_p = [(D/t)(5/4 - \mu) / E] + 1/\beta = (1.9D / 2Et) + 1/\beta$		
$\Delta P$ = Liquid Pressure Change				And:	$K_I = 3a - g$		
$\Delta T$ = Liquid Temperature Change				L = Pipe Length	t = Pipe Wall Thickness		
$\Delta V$ = Liquid Volume Added to Inside of Pipe (Negative if Flows Out)				$\mu$ = Poisson's Ratio = 0.3	E = Young's Modulus = 30x10 <sup>6</sup> psi		
V = Nominal Pipeline Volume ( $\pi D^2 L / 4$ )				$\beta$ = Liquid Bulk Modulus, a function of Press & Temp	g = Liquid Volumetric Expansion Coefficient, a Function of Press & Temp		
D = Inside Pipe Diameter				a = Linear Coefficient of Thermal Expansion	Note: Modulus of Elasticity = Young's Modulus = Elastic Modulus		
Test Medium:	Water			Pipe Material:	Carbon Steel		
API Gravity: (141.5/SG)-131.5	Specific Gravity, SG 141.5/(131.5+Degrees API)	p (SG x 1000)	(Liquid Coefficient of Expansion) B & g =	Compressibility: C = (1/B)	(Young's Modulus) E =	Linear Coefficient of Expansion: a =	
10.00	0.9990	999.012	1.23E-04	3.11E-06	2.95E+07	6.50E-06	
Pipe Data				Test Date	6/25/2014	API Gravity	10.00
Pipe Segment	$\emptyset$ Outside (in)	$\emptyset$ Inside (in)	Wall (in)	Length (ft)	Volume (Gal)	Configuration	
Non Exposed	18	17.250	0.375	58	704.15	Buried	
Nozzle Inside Tank	18	17.250	0.375	3	36.42	Inside	
Nozzle Outside Tank	12.75	12.000	0.375	4	23.50	Inside	
				Totals	65	764.07	
Weighting for Pipeline Segment			% Total Length	Configuration	Buried	Exposed	Inside
Non Exposed			0.92	Buried	0.92		
Nozzle Inside Tank			0.05	Inside			0.05
Nozzle Outside Tank			0.03	Inside			0.03
Sum of Factors			1.00	Weight Factors	0.92		0.08
The above factors are used for weighting segment temperatures							
Corrected Temperatures							
Initial Test Temperatures							
Buried	Exposed	Inside	Initial Corrected T1	DT1	AVG. T		
79.84	79.844		73.58	13.5716816	73.54		
Final Test Temperatures							
Buried	Exposed	Inside	Final Corrected T2	DT2			
79.75	79.754		73.59	13.4887396			
Corrected Temperature Difference			-0.08				
NOTE: PIPE TYPE							
Carbon Steel	E	a					
	2.95E+07	6.50E-06					
Stainless Steel	2.8E+07	9.60E-06					
FRP	2.3E+06	1.16E-05					
Aluminum	1.00E+07						
Test Pressure Difference							
Initial Pressure P1	Final Pressure P2	dPressure					
165.2	162	-3.2					
Calculate (Kp)=(1.9D/2Et)+1/B weighted value			Kp (1/P)				
Calculating C <sub>PL</sub>			C <sub>PL</sub> 1	C <sub>PL</sub> 2			
C <sub>PL</sub> = 1/(1-F <sub>p</sub> /P) or Kp (1/P)=			1.0005973	1.0005856			
Calculate (K <sub>I</sub> )=(3a-g)a-constant			Coefficient of Linear Expansion				
Calculating C <sub>TL</sub>			C <sub>TL</sub> 1	C <sub>TL</sub> 2	Temperature Correction Factor (a)	Test Duration	
C <sub>TL</sub> = Exp(-a <sub>0</sub> DT*(1+0.8a <sub>0</sub> (DT+5 <sub>0</sub> ))) or K <sub>I</sub> (1/F)=			0.9955024	0.9955299	a	a <sub>0</sub>	Hours
					6.50E-06	3.31E-04	4.00
Calculating Fluid Volume Gain/ Loss							
dV = V2-V1 = V0(C <sub>PL</sub> 2 C <sub>TL</sub> 2) - V0(C <sub>PL</sub> 1 C <sub>TL</sub> 1)			dV = Total Pipeline Volume * (Kp * dP + Ki * dT)		Net Volume Removed (Accountable Loss(-) / Gain(+)) - From Log Sheet		Unaccountable Loss
			$\Delta V / V = \text{Total Pipeline Volume } K_p \Delta P + K_I \Delta T$				Actual Gain(+)/ Loss(-)
Volume, Loss/hrs			-0.01	+			-0.01
Volume, Loss/hour			0.00	+			0.00
CSFM Loss Allowable							
Gal/hour			1.02	Gal/8hours	8.17		



**PIPELINE PETROLEUM SERVICES, INC.**

**Hydrostatic Test Volume Change Calculations (Attachment C) Page 2 of 2**

Test ID Number:	14-332-02	Code Color:	None
Customer:	Willbros Government Services	Date:	6/25/2014
System Under Evaluation:	Tank 5 Fuel Piping - 18"	Location:	Red Hill Fuel Farm, Naval Station Pearl Harbor

*Volume Change Calculations for Jet Fuel Pipeline (measured volume/pressure slope method)*

Pipe Data	Test Date	6/25/2014	API Gravity	10		
Pipe Segment	Ø Outside (in)	Ø Inside (in)	Wall (in)	Length (Ft)	Volume (Gal)	Configuration
Non Exposed	.18	17.250	0.375	58	704.15	Buried
Nozzle Inside Tank	.18	17.250	0.375	3	36.42	Inside
Nozzle Outside Tank	12.75	12.000	0.375	4	23.50	Inside
				<b>Totals</b>	<b>65</b>	<b>764.07</b>

Weighting for segment	% Total Length	Configuration	Buried	Exposed	Inside
Non Exposed	0.92	Buried	0.92		
Nozzle Inside Tank	0.05	Inside			0.05
Nozzle Outside Tank	0.03	Inside			0.03
<b>Sum of Factors</b>			<b>1.00</b>	<b>Weight Factors</b>	
			<b>0.92</b>		<b>0.05</b>

The above factors are used for weighting segment temperatures.

Corrected Temperatures					
Initial Test Temperatures					
Buried	Exposed	Inside	Initial Corrected	DT1	
79.84	79.944		73.58	13.5716816	AVG. T
					73.54
Final Test Temperatures					
Buried	Exposed	Inside	Final Corrected	DT2	
79.75	79.754		73.50	13.4887395	

Corrected Temperature Difference	<b>-0.08</b>
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Test Pressure Difference			
Initial Pressure	Final Pressure	dPressure	AVG. Pressure
165.2	162	-3.2	163.6
Use Reference from Test Data			

dV/dP Slope Calculations (Values are From Test Data)				
Initial Pressure	Final Pressure	Initial Vol.	Final Vol.	dV/dP
	165.2		2.52	0.015254237

Calculating K <sub>T</sub>				Test Duration
K <sub>T</sub> = 3a - α <sub>20</sub>	K <sub>T</sub>	Coefficient Of Linear Expansion	Temperature Correction Factor	Hours
	-0.0003115	a	α <sub>20</sub>	4.00
		6.50E-06	3.31E-04	

Calculating Fluid Volume Gain / Loss						
dV = Total Pipeline Volume * K <sub>T</sub> * dT + dV/dP * dP	dV		Net Volume Removed (Accountable Loss(-)/ Gain(+)) - From Log Sheet		Unaccountable Loss	Actual Gain(+) / Loss(-)
Volume Loss/8hrs	-0.01	+		=	-0.01	
Volume Loss/hour	0.00	+		=	0.00	
Added or Subtracted During Test						

CSFM Loss Allowable				Test Conclusion IAW CSFM / hr	
Gal./hour	1.02	Gal/8hours	8.17		<b>Pass</b>
				Test Conclusion IAW CSFM / 8 hrs	<b>Pass</b>

Note: Use this pass/fail criteria to assist in determining a successful test with the temperature evaluation.

PIPELINE PETROLEUM SERVICES, INC.

Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI

**APPENDIX D –**

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***RAW TEST DATA FROM DATALOGGER – 32" F-76 LINE***  
***RAW TEST DATA FROM DATALOGGER – 18" JP-8 LINE***

Tank 5 - 5Z - Line Test Data

Note: Pressure and Temperature readings are listed approximately every minute. Note: Times highlighted in yellow are the official test period from 17:00 to 17:12 midnight. Readings highlighted in blue are where the pressure appeared to stabilize during a 42 minute period.

Device Name: Pressure Recorder with LCD Display NBRASR Press Unit 2		Channel 1 Absolute Pressure (PSIA)		Channel 2 Thermocouple Temperature Recorder NBR127 Amb Temp 3		Channel 3 Thermocouple Temperature Recorder NBR275 Temp Unit 2	
Reading Number	Date and Time (MST)	Column 1	Column 2	Reading Number	Date and Time (MST)	Column 1	Column 2
1	2014-06-26 11:30:32	29.7	81.55	1	2014-06-26 11:30:52	79.826	80.144
2	2014-06-26 11:31:02	13.95	81.55	2	2014-06-26 11:31:52	2498	80.144
3	2014-06-26 11:31:32	13.95	81.55	3	2014-06-26 11:32:52	2498	80.144
4	2014-06-26 11:32:02	18.6	81.55	4	2014-06-26 11:33:52	2498	80.144
5	2014-06-26 11:32:32	18.6	81.55	5	2014-06-26 11:34:52	2498	80.144
6	2014-06-26 11:33:02	18.6	81.55	6	2014-06-26 11:35:52	2498	80.144
7	2014-06-26 11:33:32	18.6	81.55	7	2014-06-26 11:36:52	2498	80.144
8	2014-06-26 11:34:02	18.6	81.55	8	2014-06-26 11:37:52	2498	80.144
9	2014-06-26 11:34:32	18.6	81.55	9	2014-06-26 11:38:52	2498	80.144
10	2014-06-26 11:35:02	18.6	81.55	10	2014-06-26 11:39:52	2498	80.144
11	2014-06-26 11:35:32	18.6	81.55	11	2014-06-26 11:40:52	2498	80.144
12	2014-06-26 11:36:02	60.2	81.55	12	2014-06-26 11:41:52	79.898	80.144
13	2014-06-26 11:36:32	62.75	81.55	13	2014-06-26 11:42:52	79.898	80.144
14	2014-06-26 11:37:02	62.75	81.55	14	2014-06-26 11:43:52	79.898	80.144
15	2014-06-26 11:37:32	62.75	81.55	15	2014-06-26 11:44:52	79.898	80.144
16	2014-06-26 11:38:02	62.75	81.55	16	2014-06-26 11:45:52	79.898	80.144
17	2014-06-26 11:38:32	62.75	81.55	17	2014-06-26 11:46:52	79.898	80.144
18	2014-06-26 11:39:02	62.75	81.55	18	2014-06-26 11:47:52	79.898	80.144
19	2014-06-26 11:39:32	62.75	81.55	19	2014-06-26 11:48:52	79.898	80.144
20	2014-06-26 11:40:02	62.75	81.55	20	2014-06-26 11:49:52	79.898	80.144
21	2014-06-26 11:40:32	62.75	81.55	21	2014-06-26 11:50:52	79.898	80.144
22	2014-06-26 11:41:02	62.75	81.55	22	2014-06-26 11:51:52	79.898	80.144
23	2014-06-26 11:41:32	62.75	81.55	23	2014-06-26 11:52:52	79.898	80.144
24	2014-06-26 11:42:02	11.05	81.55	24	2014-06-26 11:53:52	79.898	80.144
25	2014-06-26 11:42:32	13.1	81.55	25	2014-06-26 11:54:52	79.898	80.144
26	2014-06-26 11:43:02	13.15	81.55	26	2014-06-26 11:55:52	79.898	80.144
27	2014-06-26 11:43:32	13.2	81.55	27	2014-06-26 11:56:52	79.898	80.144
28	2014-06-26 11:44:02	13.2	81.55	28	2014-06-26 11:57:52	79.898	80.144
29	2014-06-26 11:44:32	13.2	81.55	29	2014-06-26 11:58:52	79.898	80.144
30	2014-06-26 11:45:02	13.2	81.55	30	2014-06-26 11:59:52	79.898	80.144
31	2014-06-26 11:45:32	13.2	81.55	31	2014-06-26 12:00:52	79.898	80.144
32	2014-06-26 11:46:02	13.2	81.55	32	2014-06-26 12:01:52	79.898	80.144
33	2014-06-26 11:46:32	13.2	81.55	33	2014-06-26 12:02:52	79.898	80.144
34	2014-06-26 11:47:02	13.2	81.55	34	2014-06-26 12:03:52	79.898	80.144
35	2014-06-26 11:47:32	13.2	81.55	35	2014-06-26 12:04:52	79.898	80.144
36	2014-06-26 11:48:02	13.25	81.55	36	2014-06-26 12:05:52	79.898	80.144
37	2014-06-26 11:48:32	13.25	81.55	37	2014-06-26 12:06:52	79.898	80.144
38	2014-06-26 11:49:02	13.25	81.55	38	2014-06-26 12:07:52	79.898	80.144
39	2014-06-26 11:49:32	13.25	81.55	39	2014-06-26 12:08:52	79.898	80.144
40	2014-06-26 11:50:02	13.3	81.55	40	2014-06-26 12:09:52	79.898	80.144
41	2014-06-26 11:50:32	13.3	81.55	41	2014-06-26 12:10:52	79.898	80.144
42	2014-06-26 11:51:02	13.3	81.55	42	2014-06-26 12:11:52	79.898	80.144
43	2014-06-26 11:51:32	13.3	81.55	43	2014-06-26 12:12:52	79.898	80.144
44	2014-06-26 11:52:02	13.3	81.55	44	2014-06-26 12:13:52	79.898	80.144
45	2014-06-26 11:52:32	13.25	81.55	45	2014-06-26 12:14:52	79.898	80.144
46	2014-06-26 11:53:02	13.3	81.55	46	2014-06-26 12:15:52	79.898	80.144
47	2014-06-26 11:53:32	13.3	81.55	47	2014-06-26 12:16:52	79.898	80.144
48	2014-06-26 11:54:02	13.3	81.55	48	2014-06-26 12:17:52	79.898	80.144
49	2014-06-26 11:54:32	13.3	81.55	49	2014-06-26 12:18:52	79.898	80.144
50	2014-06-26 11:55:02	13.3	81.55	50	2014-06-26 12:19:52	79.898	80.144
51	2014-06-26 11:55:32	13.3	81.55	51	2014-06-26 12:20:52	79.898	80.144
52	2014-06-26 11:56:02	13.3	81.55	52	2014-06-26 12:21:52	79.898	80.144
53	2014-06-26 11:56:32	13.3	81.55	53	2014-06-26 12:22:52	79.898	80.144
54	2014-06-26 11:57:02	13.3	81.55	54	2014-06-26 12:23:52	79.898	80.144
55	2014-06-26 11:57:32	13.35	81.55	55	2014-06-26 12:24:52	79.898	80.144
56	2014-06-26 11:58:02	13.35	81.55	56	2014-06-26 12:25:52	79.898	80.144
57	2014-06-26 11:58:32	13.35	81.55	57	2014-06-26 12:26:52	79.898	80.144
58	2014-06-26 11:59:02	13.35	81.55	58	2014-06-26 12:27:52	79.898	80.144
59	2014-06-26 11:59:32	13.3	81.55	59	2014-06-26 12:28:52	79.898	80.144
60	2014-06-26 11:59:52	13.3	81.55	60	2014-06-26 12:29:52	79.898	80.144
61	2014-06-26 12:00:22	13.3	81.55	61	2014-06-26 12:30:52	79.898	80.144
62	2014-06-26 12:00:52	13.35	81.55	62	2014-06-26 12:31:52	79.898	80.144
63	2014-06-26 12:01:22	13.35	81.55	63	2014-06-26 12:32:52	79.898	80.144
64	2014-06-26 12:01:52	13.35	81.55	64	2014-06-26 12:33:52	79.898	80.144
65	2014-06-26 12:02:22	13.35	81.55	65	2014-06-26 12:34:52	79.898	80.144
66	2014-06-26 12:02:52	13.35	81.55	66	2014-06-26 12:35:52	79.898	80.144
67	2014-06-26 12:03:22	13.35	81.55	67	2014-06-26 12:36:52	79.898	80.144
68	2014-06-26 12:03:52	13.35	81.55	68	2014-06-26 12:37:52	79.898	80.144
69	2014-06-26 12:04:22	13.35	81.55	69	2014-06-26 12:38:52	79.898	80.144
70	2014-06-26 12:04:52	13.35	81.55	70	2014-06-26 12:39:52	79.898	80.144
71	2014-06-26 12:05:22	13.35	81.55	71	2014-06-26 12:40:52	79.898	80.144
72	2014-06-26 12:05:52	13.35	81.55	72	2014-06-26 12:41:52	79.898	80.144
73	2014-06-26 12:06:22	13.35	81.55	73	2014-06-26 12:42:52	79.898	80.144
74	2014-06-26 12:06:52	13.35	81.55	74	2014-06-26 12:43:52	79.898	80.144
75	2014-06-26 12:07:22	13.35	81.55	75	2014-06-26 12:44:52	79.898	80.144
76	2014-06-26 12:07:52	13.35	81.55	76	2014-06-26 12:45:52	79.898	80.144
77	2014-06-26 12:08:22	13.35	81.55	77	2014-06-26 12:46:52	79.898	80.144
78	2014-06-26 12:08:52	13.35	81.55	78	2014-06-26 12:47:52	79.898	80.144
79	2014-06-26 12:09:22	13.35	81.55	79	2014-06-26 12:48:52	79.898	80.144
80	2014-06-26 12:09:52	13.35	81.55	80	2014-06-26 12:49:52	79.898	80.144
81	2014-06-26 12:10:22	13.35	81.55	81	2014-06-26 12:50:52	79.898	80.144
82	2014-06-26 12:10:52	13.35	81.55	82	2014-06-26 12:51:52	79.898	80.144
83	2014-06-26 12:11:22	13.35	81.55	83	2014-06-26 12:52:52	79.898	80.144









































1318	2014-06-27/09-30/23	172.1	162.4	1119	2014-06-27/09-30/23	79.7	79.34	1315	2014-06-27/09-30/23	79.718
1319	2014-06-27/09-30/23	30.2	19.9	1320	2014-06-27/09-30/23	79.7	79.34	1321	2014-06-27/09-30/23	79.718
1320	2014-06-27/09-30/23	13.8	-0.9	1321	2014-06-27/09-30/23	79.7	79.34	1322	2014-06-27/09-30/23	79.718
1321	2014-06-27/09-30/23	11.65	-1.05	1322	2014-06-27/09-30/23	79.808	79.448	1323	2014-06-27/09-30/23	2488
1322	2014-06-27/09-30/23	11.85	-2.85	1323	2014-06-27/09-30/23	79.7	79.34	1324	2014-06-27/09-30/23	80.006
1323	2014-06-27/09-30/23	23	-2.7	1324	2014-06-27/09-30/23	79.7	79.34	1325	2014-06-27/09-30/23	80.006
1324	2014-06-27/09-30/23	15.7	-1.5	1325	2014-06-27/09-30/23	79.7	79.34	1326	2014-06-27/09-30/23	80.006
1325	2014-06-27/09-30/23	12.4	-2.4	1326	2014-06-27/09-30/23	79.7	79.34	1327	2014-06-27/09-30/23	80.006
1326	2014-06-27/09-30/23	12.5	-2.2	1327	2014-06-27/09-30/23	79.7	79.34	1328	2014-06-27/09-30/23	80.006
1327	2014-06-27/09-30/23	18	3.3	1328	2014-06-27/09-30/23	79.7	79.34	1329	2014-06-27/09-30/23	80.006
1328	2014-06-27/09-30/23	14.45	-0.25	1329	2014-06-27/09-30/23	79.808	79.448	1330	2014-06-27/09-30/23	80.006
1329	2014-06-27/09-30/23	12.45	-2.25	1330	2014-06-27/09-30/23	79.808	79.448	1331	2014-06-27/09-30/23	80.006
1330	2014-06-27/09-30/23	12.45	-2.25	1331	2014-06-27/09-30/23	80.006	80.006	1332	2014-06-27/09-30/23	80.006
1331	2014-06-27/09-30/23	12.45	-2.25	1332	2014-06-27/09-30/23	80.006	80.006	1333	2014-06-27/09-30/23	80.006
1332	2014-06-27/09-30/23	12.15	-2.55	1333	2014-06-27/09-30/23	80.006	80.006	1334	2014-06-27/09-30/23	80.006
1333	2014-06-27/09-30/23	12.25	-2.65	1334	2014-06-27/09-30/23	80.006	80.006	1335	2014-06-27/09-30/23	80.006
1334	2014-06-27/09-30/23	12.35	-2.55	1335	2014-06-27/09-30/23	81.032	2488	1336	2014-06-27/09-30/23	80.006
1335	2014-06-27/09-30/23	12.45	-2.25	1336	2014-06-27/09-30/23	81.706	2488	1337	2014-06-27/09-30/23	80.006
1336	2014-06-27/09-30/23	12.5	-2.3	1337	2014-06-27/09-30/23	81.5	2488	1338	2014-06-27/09-30/23	80.006
1337	2014-06-27/09-30/23	12.55	-2.35	1338	2014-06-27/09-30/23	81.716	2488	1339	2014-06-27/09-30/23	80.006
1338	2014-06-27/09-30/23	12.65	-2.45	1339	2014-06-27/09-30/23	81.5	2488	1340	2014-06-27/09-30/23	80.006
1339	2014-06-27/09-30/23	12.75	-2.55	1340	2014-06-27/09-30/23	82.508	2488	1341	2014-06-27/09-30/23	80.006
1340	2014-06-27/09-30/23	12.85	-2.65	1341	2014-06-27/09-30/23	82.724	2488	1342	2014-06-27/09-30/23	80.006
1341	2014-06-27/09-30/23	12.95	-2.75	1342	2014-06-27/09-30/23	82.938	2488	1343	2014-06-27/09-30/23	80.006
1342	2014-06-27/09-30/23	13.05	-2.85	1343	2014-06-27/09-30/23	83.152	2488	1344	2014-06-27/09-30/23	80.006
1343	2014-06-27/09-30/23	13.15	-2.95	1344	2014-06-27/09-30/23	83.366	2488	1345	2014-06-27/09-30/23	80.006
1344	2014-06-27/09-30/23	13.25	-3.05	1345	2014-06-27/09-30/23	83.580	2488	1346	2014-06-27/09-30/23	80.006
1345	2014-06-27/09-30/23	13.35	-3.15					1347	2014-06-27/09-30/23	80.006

Tank 5: 18" Line Test Data

Note: Pressure and temperature readings are listed approximately every minute.

Device Name: P2000 Device Description: Pressure Recorder with LCD Display Serial Number: N86436 Device ID: Press Unit 2				Device Name: QuadTemp Device Description: 4 Channel Thermocouple Temperature Recorder Serial Number: N86275 Device ID: Temp Unit 2				Device Name: TCTemp2000 Device Description: Thermocouple Temperature Recorder Serial Number: N84145 Device ID: Aux Temp 1			
Location: Flange in Lower Access Tunnel				Location: Lower Access Tunnel				Location: Inside Tank 5 on Flange			
Channel 1				Channel 2				Channel 1			
Reading Number	Date and Time (HST)	Absolute Pressure (PSIA)	Gauge Pressure (PSIG)(A-14.7)	Reading Number	Date and Time (HST)	Thermocouple 1 (Ambient) (°F)	Thermocouple 2 (AG Pipe) (°F)	Reading Number	Date and Time (HST)	Ambient Temperature (°F)	Thermocouple 1 (°F)
Column1	Column2	Column3	Column4	Column5	Column6	Column7	Column8	Column9	Column10	Column11	Column12
1	2014-06-25 07:22:17	16.7	2	1	2014-06-25 07:22:23	81.896	83.066	1	2014-06-25 07:22:04	74.966	77.846
2	2014-06-25 07:23:17	16.65	1.95	2	2014-06-25 07:23:23	81.536	82.85	2	2014-06-25 07:23:04	75.416	78.692
3	2014-06-25 07:24:17	16.65	1.95	3	2014-06-25 07:24:53	80.87	82.616	3	2014-06-25 07:24:34	75.758	79.124
4	2014-06-25 07:25:17	16.65	1.95	4	2014-06-25 07:25:53	80.726	82.472	4	2014-06-25 07:25:34	75.974	79.374
5	2014-06-25 07:26:17	16.65	1.95	5	2014-06-25 07:26:53	80.576	82.328	5	2014-06-25 07:26:34	76.1	79.376
6	2014-06-25 07:27:17	16.6	1.9	6	2014-06-25 07:27:53	80.492	82.148	6	2014-06-25 07:27:34	76.208	79.417
7	2014-06-25 07:28:17	16.65	1.95	7	2014-06-25 07:28:53	80.348	81.958	7	2014-06-25 07:28:34	76.55	79.664
8	2014-06-25 07:29:17	16.6	1.9	8	2014-06-25 07:29:53	80.402	81.968	8	2014-06-25 07:29:34	76.658	79.678
9	2014-06-25 07:30:17	16.6	1.9	9	2014-06-25 07:30:53	80.33	81.824	9	2014-06-25 07:30:34	76.874	79.718
10	2014-06-25 07:31:17	23.4	8.7	10	2014-06-25 07:31:53	80.24	81.662	10	2014-06-25 07:31:34	77	79.754
11	2014-06-25 07:32:17	63.1	48.4	11	2014-06-25 07:32:53	80.168	81.572	11	2014-06-25 07:32:34	77.108	79.736
12	2014-06-25 07:33:17	22.4	7.7	12	2014-06-25 07:33:23	80.186	81.626	12	2014-06-25 07:33:04	77.216	79.754
13	2014-06-25 07:34:17	30.45	15.75	13	2014-06-25 07:34:53	80.132	81.41	13	2014-06-25 07:34:34	77.45	79.772
14	2014-06-25 07:35:17	41.3	26.6	14	2014-06-25 07:35:53	80.132	81.464	14	2014-06-25 07:35:34	77.45	79.782
15	2014-06-25 07:36:17	53.2	38.5	15	2014-06-25 07:36:53	80.078	81.338	15	2014-06-25 07:36:34	77.666	79.808
16	2014-06-25 07:37:17	60.2	45.5	16	2014-06-25 07:37:53	80.06	81.302	16	2014-06-25 07:37:34	77.666	79.772
17	2014-06-25 07:38:17	61.85	47.15	17	2014-06-25 07:38:53	80.132	81.266	17	2014-06-25 07:38:34	77.774	79.754
18	2014-06-25 07:39:17	70.75	56.05	18	2014-06-25 07:39:53	80.096	81.194	18	2014-06-25 07:39:34	77.9	79.826
19	2014-06-25 07:40:17	117.65	102.95	19	2014-06-25 07:40:53	80.078	81.176	19	2014-06-25 07:40:34	77.9	79.882
20	2014-06-25 07:41:17	117.25	102.55	20	2014-06-25 07:41:53	80.096	81.104	20	2014-06-25 07:41:34	78.008	79.79
21	2014-06-25 07:42:17	106	91.3	21	2014-06-25 07:42:53	80.078	81.05	21	2014-06-25 07:42:34	78.116	79.61
22	2014-06-25 07:43:17	143.2	128.5	22	2014-06-25 07:43:53	80.132	81.014	22	2014-06-25 07:43:34	78.35	79.628
23	2014-06-25 07:44:17	178.35	163.65	23	2014-06-25 07:44:53	80.15	81.014	23	2014-06-25 07:44:34	78.458	79.666
24	2014-06-25 07:45:17	178.05	163.35	24	2014-06-25 07:45:53	80.186	80.564	24	2014-06-25 07:45:34	78.566	79.574
25	2014-06-25 07:46:17	177.85	163.15	25	2014-06-25 07:46:53	80.15	80.448	25	2014-06-25 07:46:34	78.674	79.502
26	2014-06-25 07:47:17	177.7	163	26	2014-06-25 07:47:53	80.204	80.528	26	2014-06-25 07:47:34	78.808	79.61
27	2014-06-25 07:48:17	177.55	162.85	27	2014-06-25 07:48:53	80.15	80.51	27	2014-06-25 07:48:34	79.016	79.592
28	2014-06-25 07:49:17	177.35	162.65	28	2014-06-25 07:49:53	80.114	80.51	28	2014-06-25 07:49:34	79.124	79.574
29	2014-06-25 07:50:17	177.25	162.55	29	2014-06-25 07:50:53	80.114	80.492	29	2014-06-25 07:50:34	79.25	79.561
30	2014-06-25 07:51:17	177.15	162.45	30	2014-06-25 07:51:53	80.114	80.528	30	2014-06-25 07:51:34	79.25	79.52
31	2014-06-25 07:52:17	177	162.3	31	2014-06-25 07:52:53	80.096	80.492	31	2014-06-25 07:52:34	79.358	79.538
32	2014-06-25 07:53:17	176.85	162.15	32	2014-06-25 07:53:53	80.402	80.528	32	2014-06-25 07:53:34	79.358	79.502
33	2014-06-25 07:54:17	176.75	162.05	33	2014-06-25 07:54:53	80.402	80.474	33	2014-06-25 07:54:34	79.358	79.412
34	2014-06-25 07:55:17	176.65	161.95	34	2014-06-25 07:55:53	80.366	80.438	34	2014-06-25 07:55:34	79.466	79.43
35	2014-06-25 07:56:17	176.55	161.85	35	2014-06-25 07:56:53	80.294	80.47	35	2014-06-25 07:56:34	79.466	79.43
36	2014-06-25 07:57:17	176.45	161.75	36	2014-06-25 07:57:53	80.186	80.456	36	2014-06-25 07:57:34	79.574	79.448
37	2014-06-25 07:58:17	174.75	160.05	37	2014-06-25 07:58:53	80.186	80.366	37	2014-06-25 07:58:34	79.7	79.574
38	2014-06-25 07:59:17	15.35	0.65	38	2014-06-25 07:59:53	80.15	80.366	38	2014-06-25 07:59:34	79.7	79.538
39	2014-06-25 08:00:17	173.65	157.95	39	2014-06-25 08:00:53	80.06	80.402	39	2014-06-25 08:00:34	79.7	79.484
40	2014-06-25 08:01:17	165.15	150.45	40	2014-06-25 08:01:53	80.096	80.366	40	2014-06-25 08:01:34	79.7	79.448
41	2014-06-25 08:02:17	159.25	144.55	41	2014-06-25 08:02:53	80.042	80.402	41	2014-06-25 08:02:34	79.808	79.466
42	2014-06-25 08:03:17	173.35	158.65	42	2014-06-25 08:03:53	80.06	80.366	42	2014-06-25 08:03:34	79.808	79.466
43	2014-06-25 08:04:17	173.4	158.6	43	2014-06-25 08:04:53	80.024	80.366	43	2014-06-25 08:04:34	79.808	79.412
44	2014-06-25 08:05:17	173.2	158.5	44	2014-06-25 08:05:53	80.024	80.33	44	2014-06-25 08:05:34	79.916	79.52
45	2014-06-25 08:06:17	173.15	158.45	45	2014-06-25 08:06:53	80.024	80.348	45	2014-06-25 08:06:34	79.916	79.484
46	2014-06-25 08:07:17	178.25	163.55	46	2014-06-25 08:07:53	79.988	80.33	46	2014-06-25 08:07:34	79.916	79.484
47	2014-06-25 08:08:17	178.2	163.5	47	2014-06-25 08:08:53	80.024	80.294	47	2014-06-25 08:08:34	79.916	79.484
48	2014-06-25 08:09:17	178.1	163.4	48	2014-06-25 08:09:53	80.024	80.33	48	2014-06-25 08:09:34	79.916	79.394
49	2014-06-25 08:10:17	178	163.3	49	2014-06-25 08:10:53	80.042	80.33	49	2014-06-25 08:10:34	80.024	79.502
50	2014-06-25 08:11:17	177.95	163.25	50	2014-06-25 08:11:53	80.06	80.276	50	2014-06-25 08:11:34	79.916	79.502
51	2014-06-25 08:12:17	177.9	163.2	51	2014-06-25 08:12:53	80.024	80.276	51	2014-06-25 08:12:34	79.916	79.268
52	2014-06-25 08:13:17	177.85	163.15	52	2014-06-25 08:13:53	80.024	80.276	52	2014-06-25 08:13:34	80.024	79.412
53	2014-06-25 08:14:17	177.75	163.05	53	2014-06-25 08:14:53	80.024	80.294	53	2014-06-25 08:14:34	80.024	79.412
54	2014-06-25 08:15:17	177.7	163	54	2014-06-25 08:15:53	80.078	80.204	54	2014-06-25 08:15:34	80.024	79.376
55	2014-06-25 08:16:17	177.65	162.95	55	2014-06-25 08:16:53	80.096	80.294	55	2014-06-25 08:16:34	80.024	79.376
56	2014-06-25 08:17:17	177.55	162.85	56	2014-06-25 08:17:53	80.042	80.33	56	2014-06-25 08:17:34	80.024	79.376
57	2014-06-25 08:18:17	177.5	162.8	57	2014-06-25 08:18:53	80.06	80.276	57	2014-06-25 08:18:34	80.024	79.376
58	2014-06-25 08:19:17	177.45	162.75	58	2014-06-25 08:19:53	80.078	80.276	58	2014-06-25 08:19:34	80.15	79.448
59	2014-06-25 08:20:17	177.35	162.65	59	2014-06-25 08:20:53	80.078	80.24	59	2014-06-25 08:20:34	80.15	79.412
60	2014-06-25 08:21:17	177.3	162.6	60	2014-06-25 08:21:53	80.078	80.258	60	2014-06-25 08:21:34	80.15	79.376
61	2014-06-25 08:22:17	177.25	162.55	61	2014-06-25 08:22:53	80.042	80.222	61	2014-06-25 08:22:34	80.15	79.376
62	2014-06-25 08:23:17	176.05	161.35	62	2014-06-25 08:23:53	80.096	80.272	62	2014-06-25 08:23:34	80.258	79.34
63	2014-06-25 08:24:17	175.65	160.95	63	2014-06-25 08:24:53	80.042	80.204	63	2014-06-25 08:24:34	80.258	79.124
64	2014-06-25 08:25:17	175.6	160.9	64	2014-06-25 08:25:53	80.096	80.204	64	2014-06-25 08:25:34	80.366	79.016
65	2014-06-25 08:26:17	176.5	161.8	65	2014-06-25 08:26:53	80.078	80.168	65	2014-06-25 08:26:34	80.366	78.89
66	2014-06-25 08:27:17	177	162.3	66	2014-06-25 08:27:53	80.042	80.222	66	2014-06-25 08:27:34	80.366	78.98
67	2014-06-25 08:28:17	65.45	50.75	67	2014-06-25 08:28:53	80.078	80.272	67	2014-06-25 08:28:34	80.366	78.98
68	2014-06-25 08:29:17	14.95	0.25	68	2014-06-25 08:29:53	80.15	80.168	68	2014-06-25 08:29:34	80.366	78.98
69	2014-06-25 08:30:17	14.95	0.25	69	2014-06-25 08:30:53	80.024	80.168	69	2014-06-25 08:30:34	80.366	78.98
70	2014-06-25 08:31:17	14.95	0.25	70	2014-06-25 08:31:53	80.06	80.276	70	2014-06-25 08:31:34	80.474	79.08
71	2014-06-25 08:32:17	14.95	0.25	71	2014-06-25 08:32:53	80.06	80.204	71	2014-06-25 08:32:34	80.474	79.034
72	2014-06-25 08:33:17	14.95	0.25	72	2014-06-25 08:33:53	80.024	80.168	72	2014-06-25 08:33:34	80.474	78.998



73	2014-06-25 08:30:17	15	73	0	73	2014-06-25 08:34:53	80,024	80,155	2014-06-25 08:34:53	73	80,366	78,886
74	2014-06-25 08:30:17	17,65	74	2,95	74	2014-06-25 08:35:53	80,024	80,204	2014-06-25 08:35:53	74	80,366	78,886
75	2014-06-25 08:30:17	18,85	75	4,25	75	2014-06-25 08:36:53	80,042	80,222	2014-06-25 08:36:53	75	80,474	79,508
76	2014-06-25 08:30:17	18,85	76	4,13	76	2014-06-25 08:37:53	79,988	80,168	2014-06-25 08:37:53	76	80,366	78,886
77	2014-06-25 08:30:17	18,85	77	4,13	77	2014-06-25 08:38:53	80,115	80,295	2014-06-25 08:38:53	77	80,474	79,508
78	2014-06-25 08:30:17	18,85	78	4,05	78	2014-06-25 08:39:53	80,142	80,322	2014-06-25 08:39:53	78	80,366	78,886
79	2014-06-25 08:30:17	18,85	79	4,05	79	2014-06-25 08:40:53	80,169	80,349	2014-06-25 08:40:53	79	80,474	79,508
80	2014-06-25 08:30:17	18,7	80	4	80	2014-06-25 08:41:53	80,196	80,376	2014-06-25 08:41:53	80	80,366	78,886
81	2014-06-25 08:30:17	18,7	81	3,96	81	2014-06-25 08:42:53	80,223	80,403	2014-06-25 08:42:53	81	80,474	79,508
82	2014-06-25 08:30:17	18,65	82	3,84	82	2014-06-25 08:43:53	80,250	80,430	2014-06-25 08:43:53	82	80,366	78,886
83	2014-06-25 08:30:17	18,6	83	3,84	83	2014-06-25 08:44:53	80,277	80,457	2014-06-25 08:44:53	83	80,474	79,508
84	2014-06-25 08:30:17	18,6	84	3,9	84	2014-06-25 08:45:53	80,304	80,484	2014-06-25 08:45:53	84	80,366	78,886
85	2014-06-25 08:30:17	18,6	85	3,9	85	2014-06-25 08:46:53	80,331	80,511	2014-06-25 08:46:53	85	80,474	79,508
86	2014-06-25 08:30:17	18,6	86	3,85	86	2014-06-25 08:47:53	80,358	80,538	2014-06-25 08:47:53	86	80,366	78,886
87	2014-06-25 08:30:17	18,55	87	3,85	87	2014-06-25 08:48:53	80,385	80,565	2014-06-25 08:48:53	87	80,474	79,508
88	2014-06-25 08:30:17	18,6	88	3,9	88	2014-06-25 08:49:53	80,412	80,592	2014-06-25 08:49:53	88	80,366	78,886
89	2014-06-25 08:30:17	18,6	89	3,9	89	2014-06-25 08:50:53	80,439	80,619	2014-06-25 08:50:53	89	80,474	79,508
90	2014-06-25 08:30:17	18,6	90	3,9	90	2014-06-25 08:51:53	80,466	80,646	2014-06-25 08:51:53	90	80,366	78,886
91	2014-06-25 08:30:17	18,6	91	3,9	91	2014-06-25 08:52:53	80,493	80,673	2014-06-25 08:52:53	91	80,474	79,508
92	2014-06-25 08:30:17	18,6	92	3,9	92	2014-06-25 08:53:53	80,520	80,700	2014-06-25 08:53:53	92	80,366	78,886
93	2014-06-25 08:30:17	18,6	93	3,9	93	2014-06-25 08:54:53	80,547	80,727	2014-06-25 08:54:53	93	80,474	79,508
94	2014-06-25 08:30:17	18,6	94	3,9	94	2014-06-25 08:55:53	80,574	80,754	2014-06-25 08:55:53	94	80,366	78,886
95	2014-06-25 08:30:17	18,6	95	3,9	95	2014-06-25 08:56:53	80,601	80,781	2014-06-25 08:56:53	95	80,474	79,508
96	2014-06-25 08:30:17	18,6	96	3,9	96	2014-06-25 08:57:53	80,628	80,808	2014-06-25 08:57:53	96	80,366	78,886
97	2014-06-25 08:30:17	18,6	97	3,9	97	2014-06-25 08:58:53	80,655	80,835	2014-06-25 08:58:53	97	80,474	79,508
98	2014-06-25 08:30:17	18,6	98	3,9	98	2014-06-25 08:59:53	80,682	80,862	2014-06-25 08:59:53	98	80,366	78,886
99	2014-06-25 08:30:17	18,6	99	3,9	99	2014-06-25 09:00:53	80,709	80,889	2014-06-25 09:00:53	99	80,474	79,508
100	2014-06-25 08:30:17	18,6	100	3,9	100	2014-06-25 09:01:53	80,736	80,916	2014-06-25 09:01:53	100	80,366	78,886
101	2014-06-25 08:30:17	18,6	101	3,9	101	2014-06-25 09:02:53	80,763	80,943	2014-06-25 09:02:53	101	80,474	79,508
102	2014-06-25 08:30:17	18,6	102	3,9	102	2014-06-25 09:03:53	80,790	80,970	2014-06-25 09:03:53	102	80,366	78,886
103	2014-06-25 08:30:17	18,6	103	3,9	103	2014-06-25 09:04:53	80,817	81,000	2014-06-25 09:04:53	103	80,474	79,508
104	2014-06-25 08:30:17	18,6	104	3,9	104	2014-06-25 09:05:53	80,844	81,030	2014-06-25 09:05:53	104	80,366	78,886
105	2014-06-25 08:30:17	18,6	105	3,9	105	2014-06-25 09:06:53	80,871	81,060	2014-06-25 09:06:53	105	80,474	79,508
106	2014-06-25 08:30:17	18,6	106	3,9	106	2014-06-25 09:07:53	80,898	81,090	2014-06-25 09:07:53	106	80,366	78,886
107	2014-06-25 08:30:17	18,6	107	3,9	107	2014-06-25 09:08:53	80,925	81,120	2014-06-25 09:08:53	107	80,474	79,508
108	2014-06-25 08:30:17	18,6	108	3,9	108	2014-06-25 09:09:53	80,952	81,150	2014-06-25 09:09:53	108	80,366	78,886
109	2014-06-25 08:30:17	18,6	109	3,9	109	2014-06-25 09:10:53	80,979	81,180	2014-06-25 09:10:53	109	80,474	79,508
110	2014-06-25 08:30:17	18,6	110	3,9	110	2014-06-25 09:11:53	81,006	81,210	2014-06-25 09:11:53	110	80,366	78,886
111	2014-06-25 08:30:17	18,6	111	3,9	111	2014-06-25 09:12:53	81,033	81,240	2014-06-25 09:12:53	111	80,474	79,508
112	2014-06-25 08:30:17	18,6	112	3,9	112	2014-06-25 09:13:53	81,060	81,270	2014-06-25 09:13:53	112	80,366	78,886
113	2014-06-25 08:30:17	18,6	113	3,9	113	2014-06-25 09:14:53	81,087	81,300	2014-06-25 09:14:53	113	80,474	79,508
114	2014-06-25 08:30:17	18,6	114	3,9	114	2014-06-25 09:15:53	81,114	81,330	2014-06-25 09:15:53	114	80,366	78,886
115	2014-06-25 08:30:17	18,6	115	3,9	115	2014-06-25 09:16:53	81,141	81,360	2014-06-25 09:16:53	115	80,474	79,508
116	2014-06-25 08:30:17	18,6	116	3,9	116	2014-06-25 09:17:53	81,168	81,390	2014-06-25 09:17:53	116	80,366	78,886
117	2014-06-25 08:30:17	18,6	117	3,9	117	2014-06-25 09:18:53	81,195	81,420	2014-06-25 09:18:53	117	80,474	79,508
118	2014-06-25 08:30:17	18,6	118	3,9	118	2014-06-25 09:19:53	81,222	81,450	2014-06-25 09:19:53	118	80,366	78,886
119	2014-06-25 08:30:17	18,6	119	3,9	119	2014-06-25 09:20:53	81,249	81,480	2014-06-25 09:20:53	119	80,474	79,508
120	2014-06-25 08:30:17	18,6	120	3,9	120	2014-06-25 09:21:53	81,276	81,510	2014-06-25 09:21:53	120	80,366	78,886
121	2014-06-25 08:30:17	18,6	121	3,9	121	2014-06-25 09:22:53	81,303	81,540	2014-06-25 09:22:53	121	80,474	79,508
122	2014-06-25 08:30:17	18,6	122	3,9	122	2014-06-25 09:23:53	81,330	81,570	2014-06-25 09:23:53	122	80,366	78,886
123	2014-06-25 08:30:17	18,6	123	3,9	123	2014-06-25 09:24:53	81,357	81,600	2014-06-25 09:24:53	123	80,474	79,508
124	2014-06-25 08:30:17	18,6	124	3,9	124	2014-06-25 09:25:53	81,384	81,630	2014-06-25 09:25:53	124	80,366	78,886
125	2014-06-25 08:30:17	18,6	125	3,9	125	2014-06-25 09:26:53	81,411	81,660	2014-06-25 09:26:53	125	80,474	79,508
126	2014-06-25 08:30:17	18,6	126	3,9	126	2014-06-25 09:27:53	81,438	81,690	2014-06-25 09:27:53	126	80,366	78,886
127	2014-06-25 08:30:17	18,6	127	3,9	127	2014-06-25 09:28:53	81,465	81,720	2014-06-25 09:28:53	127	80,474	79,508
128	2014-06-25 08:30:17	18,6	128	3,9	128	2014-06-25 09:29:53	81,492	81,750	2014-06-25 09:29:53	128	80,366	78,886
129	2014-06-25 08:30:17	18,6	129	3,9	129	2014-06-25 09:30:53	81,519	81,780	2014-06-25 09:30:53	129	80,474	79,508
130	2014-06-25 08:30:17	18,6	130	3,9	130	2014-06-25 09:31:53	81,546	81,810	2014-06-25 09:31:53	130	80,366	78,886
131	2014-06-25 08:30:17	18,6	131	3,9	131	2014-06-25 09:32:53	81,573	81,840	2014-06-25 09:32:53	131	80,474	79,508
132	2014-06-25 08:30:17	18,6	132	3,9	132	2014-06-25 09:33:53	81,600	81,870	2014-06-25 09:33:53	132	80,366	78,886
133	2014-06-25 08:30:17	18,6	133	3,9	133	2014-06-25 09:34:53	81,627	81,900	2014-06-25 09:34:53	133	80,474	79,508
134	2014-06-25 08:30:17	18,6	134	3,9	134	2014-06-25 09:35:53	81,654	81,930	2014-06-25 09:35:53	134	80,366	78,886
135	2014-06-25 08:30:17	18,6	135	3,9	135	2014-06-25 09:36:53	81,681	81,960	2014-06-25 09:36:53	135	80,474	79,508
136	2014-06-25 08:30:17	18,6	136	3,9	136	2014-06-25 09:37:53	81,708	81,990	2014-06-25 09:37:53	136	80,366	78,886
137	2014-06-25 08:30:17	18,6	137	3,9	137	2014-06-25 09:38:53	81,735	82,020	2014-06-25 09:38:53	137	80,474	79,508
138	2014-06-25 08:30:17	18,6	138	3,9	138	2014-06-25 09:39:53	81,762	82,050	2014-06-25 09:39:53	138	80,366	78,886
139	2014-06-25 08:30:17	18,6	139	3,9	139	2014-06-25 09:40:53	81,789	82,080	2014-06-25 09:40:53	139	80,474	79,508
140	2014-06-25 08:30:17	18,6	140	3,9	140	2014-06-25 09:41:53	81,816	82,110	2014-06-25 09:41:53	140	80,366	78,886
141	2014-06-25 08:30:17	18,6	141	3,9	141	2014-06-25 09:42:53	81,843	82,140	2014-06-25 09:42:53	141	80,474	79,508
142	2014-06-25 08:30:17	18,6	142	3,9	142	2014-06-25 09:43:53	81,870	82,170	2014-06-25 09:43:53	142	80,366	78,886
143	2014-06-25 08:30:17	18,6	143	3,9	143	2014-06-25 09:44:53	81,897	82,200	2014-06-25 09:44:53	143	80,474	79,508
144	2014-06-25 08:30:17	18,6	144	3,9	144	2014-06-25 09:45:53	81,924	82,230	2014-06-25 09:45:53	144	80,366	78,886
145	2014-06-25 08:30:17	18,6	145	3,9	145	2014-06-25 09:46:53	81,951	82,260	2014-06-25 09:46:53	145	80,474	79,508
146	2014-06-25 08:30:1											

156	2014-06-25 09:57:17	180.2	165.5	156	2014-06-25 09:57:53	79.936	80.168	156	2014-06-25 10:57:34	80.258	79.646
157	2014-06-25 09:58:17	180.35	165.9	157	2014-06-25 09:58:53	79.982	80.186	157	2014-06-25 10:58:34	80.258	79.736
158	2014-06-25 09:58:41	180.1	165.4	158	2014-06-25 09:59:53	79.826	80.168	158	2014-06-25 10:59:34	80.258	79.628
159	2014-06-25 09:59:17	180.11	165.9	159	2014-06-25 10:00:53	79.862	80.168	159	2014-06-25 10:00:34	80.258	79.628
160	2014-06-25 10:00:17	180.1	165.3	160	2014-06-25 10:01:53	79.844	80.168	160	2014-06-25 10:01:34	80.258	79.628
161	2014-06-25 10:01:41	180.1	165.3	161	2014-06-25 10:02:53	79.888	80.168	161	2014-06-25 10:02:34	80.258	79.628
162	2014-06-25 10:03:17	179.95	165.05	162	2014-06-25 10:03:53	79.888	80.168	162	2014-06-25 10:03:34	80.258	79.718
163	2014-06-25 10:04:17	179.65	165.05	163	2014-06-25 10:04:53	79.772	80.168	163	2014-06-25 10:04:34	80.258	79.718
164	2014-06-25 10:05:17	179.55	164.85	164	2014-06-25 10:05:53	79.844	80.132	164	2014-06-25 10:05:34	80.258	79.718
165	2014-06-25 10:06:17	179.35	164.65	165	2014-06-25 10:06:53	79.79	80.15	165	2014-06-25 10:06:34	80.258	79.772
166	2014-06-25 10:07:17	179.2	164.5	166	2014-06-25 10:07:53	79.844	80.096	166	2014-06-25 10:07:34	80.258	79.772
167	2014-06-25 10:08:17	179.05	164.35	167	2014-06-25 10:08:53	79.79	80.096	167	2014-06-25 10:08:34	80.258	79.772
168	2014-06-25 10:09:17	178.8	164.1	168	2014-06-25 10:09:53	79.79	80.096	168	2014-06-25 10:09:34	80.258	79.772
169	2014-06-25 10:10:17	178.45	163.9	169	2014-06-25 10:10:53	79.806	80.078	169	2014-06-25 10:10:34	80.258	79.806
170	2014-06-25 10:11:17	178.45	163.75	170	2014-06-25 10:11:53	79.806	80.096	170	2014-06-25 10:11:34	80.258	79.806
171	2014-06-25 10:12:17	178.25	163.55	171	2014-06-25 10:12:53	79.856	80.096	171	2014-06-25 10:12:34	80.258	79.806
172	2014-06-25 10:13:17	178.1	163.4	172	2014-06-25 10:13:53	79.79	80.096	172	2014-06-25 10:13:34	80.258	79.844
173	2014-06-25 10:14:17	177.85	163.25	173	2014-06-25 10:14:53	79.772	80.06	173	2014-06-25 10:14:34	80.258	79.844
174	2014-06-25 10:15:17	177.85	163.15	174	2014-06-25 10:15:53	79.79	80.06	174	2014-06-25 10:15:34	80.258	79.898
175	2014-06-25 10:16:17	177.55	162.85	175	2014-06-25 10:16:53	79.79	80.06	175	2014-06-25 10:16:34	80.258	79.934
176	2014-06-25 10:17:17	177.15	162.45	176	2014-06-25 10:17:53	79.772	80.042	176	2014-06-25 10:17:34	80.258	80.024
177	2014-06-25 10:18:17	176.7	162.1	177	2014-06-25 10:18:53	79.79	80.024	177	2014-06-25 10:18:34	80.258	80.078
178	2014-06-25 10:19:17	176.45	161.9	178	2014-06-25 10:19:53	79.808	80.024	178	2014-06-25 10:19:34	80.258	80.114
179	2014-06-25 10:20:17	176.15	161.65	179	2014-06-25 10:20:53	79.936	80.066	179	2014-06-25 10:20:34	80.258	80.024
180	2014-06-25 10:21:17	176.15	161.45	180	2014-06-25 10:21:53	79.936	80.066	180	2014-06-25 10:21:34	80.258	80.024
181	2014-06-25 10:22:17	176.15	161.3	181	2014-06-25 10:22:53	79.936	80.024	181	2014-06-25 10:22:34	80.258	80.024
182	2014-06-25 10:23:17	176.15	161.3	182	2014-06-25 10:23:53	79.936	80.024	182	2014-06-25 10:23:34	80.258	80.024
183	2014-06-25 10:24:17	176.15	161.3	183	2014-06-25 10:24:53	79.936	80.066	183	2014-06-25 10:24:34	80.258	80.024
184	2014-06-25 10:25:17	175.95	161.25	184	2014-06-25 10:25:53	79.936	80.066	184	2014-06-25 10:25:34	80.258	80.066
185	2014-06-25 10:26:17	175.95	161.25	185	2014-06-25 10:26:53	79.936	80.066	185	2014-06-25 10:26:34	80.258	80.066
186	2014-06-25 10:27:17	175.9	161.2	186	2014-06-25 10:27:53	79.79	80.066	186	2014-06-25 10:27:34	80.258	80.114
187	2014-06-25 10:28:17	175.9	161.2	187	2014-06-25 10:28:53	79.79	80.066	187	2014-06-25 10:28:34	80.258	80.114
188	2014-06-25 10:29:17	175.85	161.15	188	2014-06-25 10:29:53	79.808	80.066	188	2014-06-25 10:29:34	80.258	80.114
189	2014-06-25 10:30:17	175.85	161.15	189	2014-06-25 10:30:53	79.808	80.066	189	2014-06-25 10:30:34	80.258	80.114
190	2014-06-25 10:31:17	175.8	161.1	190	2014-06-25 10:31:53	79.772	79.916	190	2014-06-25 10:31:34	80.258	80.294
191	2014-06-25 10:32:17	175.8	161.1	191	2014-06-25 10:32:53	79.772	79.916	191	2014-06-25 10:32:34	80.258	80.294
192	2014-06-25 10:33:17	175.8	161.1	192	2014-06-25 10:33:53	79.772	79.916	192	2014-06-25 10:33:34	80.258	80.294
193	2014-06-25 10:34:17	175.75	161.05	193	2014-06-25 10:34:53	79.844	79.952	193	2014-06-25 10:34:34	80.258	80.33
194	2014-06-25 10:35:17	175.75	161.05	194	2014-06-25 10:35:53	79.79	80.066	194	2014-06-25 10:35:34	80.258	80.294
195	2014-06-25 10:36:17	175.75	161.05	195	2014-06-25 10:36:53	79.808	80.066	195	2014-06-25 10:36:34	80.258	80.33
196	2014-06-25 10:37:17	175.5	160.8	196	2014-06-25 10:37:53	79.916	79.952	196	2014-06-25 10:37:34	80.258	80.51
197	2014-06-25 10:38:17	174.9	160.2	197	2014-06-25 10:38:53	79.808	79.952	197	2014-06-25 10:38:34	80.258	80.47
198	2014-06-25 10:39:17	174.5	159.8	198	2014-06-25 10:39:53	79.808	79.952	198	2014-06-25 10:39:34	80.258	80.294
199	2014-06-25 10:40:17	174.5	159.8	199	2014-06-25 10:40:53	79.808	79.952	199	2014-06-25 10:40:34	80.258	80.294
200	2014-06-25 10:41:17	167	152	200	2014-06-25 10:41:53	79.916	79.916	200	2014-06-25 10:41:34	80.258	80.294
201	2014-06-25 10:42:17	14.55	131	201	2014-06-25 10:42:53	79.916	80.066	201	2014-06-25 10:42:34	80.258	80.312
202	2014-06-25 10:43:17	14.55	131	202	2014-06-25 10:43:53	79.916	80.066	202	2014-06-25 10:43:34	80.258	80.312
203	2014-06-25 10:44:17	14.6	131	203	2014-06-25 10:44:53	79.936	80.024	203	2014-06-25 10:44:34	80.258	80.258
204	2014-06-25 10:45:17	14.6	131	204	2014-06-25 10:45:53	79.862	80.024	204	2014-06-25 10:45:34	80.258	80.258
205	2014-06-25 10:46:17	14.6	131	205	2014-06-25 10:46:53	79.862	80.024	205	2014-06-25 10:46:34	80.258	80.258
206	2014-06-25 10:47:17	14.6	131	206	2014-06-25 10:47:53	79.772	80.066	206	2014-06-25 10:47:34	80.258	80.366
207	2014-06-25 10:48:17	14.6	131	207	2014-06-25 10:48:53	79.772	80.066	207	2014-06-25 10:48:34	80.258	80.366
208	2014-06-25 10:49:17	14.6	131	208	2014-06-25 10:49:53	79.844	80.066	208	2014-06-25 10:49:34	80.258	80.366
209	2014-06-25 10:50:17	14.6	131	209	2014-06-25 10:50:53	79.844	80.066	209	2014-06-25 10:50:34	80.258	80.366
210	2014-06-25 10:51:17	14.6	131	210	2014-06-25 10:51:53	79.844	80.066	210	2014-06-25 10:51:34	80.258	80.366
211	2014-06-25 10:52:17	14.6	131	211	2014-06-25 10:52:53	79.844	80.066	211	2014-06-25 10:52:34	80.258	80.366
212	2014-06-25 10:53:17	14.65	131	212	2014-06-25 10:53:53	79.916	80.066	212	2014-06-25 10:53:34	80.258	80.366
213	2014-06-25 10:54:17	14.65	131	213	2014-06-25 10:54:53	79.916	80.066	213	2014-06-25 10:54:34	80.258	80.366
214	2014-06-25 10:55:17	18.1	131	214	2014-06-25 10:55:53	79.79	79.916	214	2014-06-25 10:55:34	80.258	80.366
215	2014-06-25 10:56:17	18.15	131	215	2014-06-25 10:56:53	79.79	79.916	215	2014-06-25 10:56:34	80.258	80.366
216	2014-06-25 10:57:17	18.2	131	216	2014-06-25 10:57:53	79.754	79.888	216	2014-06-25 10:57:34	80.258	80.474
217	2014-06-25 10:58:17	18.25	131	217	2014-06-25 10:58:53	79.754	79.888	217	2014-06-25 10:58:34	80.258	80.474
218	2014-06-25 10:59:17	18.25	131	218	2014-06-25 10:59:53	79.79	79.888	218	2014-06-25 10:59:34	80.258	80.474
219	2014-06-25 11:00:17	18.25	131	219	2014-06-25 11:00:53	79.862	79.888	219	2014-06-25 11:00:34	80.258	80.474
220	2014-06-25 11:01:17	18.3	131	220	2014-06-25 11:01:53	79.754	79.888	220	2014-06-25 11:01:34	80.258	80.474
221	2014-06-25 11:02:17	18.3	131	221	2014-06-25 11:02:53	79.952	79.888	221	2014-06-25 11:02:34	80.258	80.474
222	2014-06-25 11:03:17	18.3	131	222	2014-06-25 11:03:53	79.916	79.916	222	2014-06-25 11:03:34	80.258	80.474
223	2014-06-25 11:04:17	18.3	131	223	2014-06-25 11:04:53	79.844	79.844	223	2014-06-25 11:04:34	80.258	80.474
224	2014-06-25 11:05:17	18.3	131	224	2014-06-25 11:05:53	79.772	79.844	224	2014-06-25 11:05:34	80.258	80.474
225	2014-06-25 11:06:17	18.3	131	225	2014-06-25 11:06:53	79.79	79.888	225	2014-06-25 11:06:34	80.258	80.474
226	2014-06-25 11:07:17	18.3	131	226	2014-06-25 11:07:53	79.754	79.888	226	2014-06-25 11:07:34	80.258	80.474
227	2014-06-25 11:08:17	18.35	131	227	2014-06-25 11:08:53	79.754	79.888	227	2014-06-25 11:08:34	80.258	80.474
228	2014-06-25 11:09:17	18.35	131	228	2014-06-25 11:09:53	79.79	79.888	228	2014-06-25 11:09:34	80.258	80.474
229	2014-06-25 11:10:17	18.35	131	229	2014-06-25 11:10:53	79.79	79.888	229	2014-06-25 11:10:34	80.258	80.474
230	2014-06-25 11:11:17	18.35	131	230	2014-06-25 11:11:53	79.79	79.888	230	2014-06-25 11:11:34	80.258	80.474
231	2014-06-25 11:12:17										

239	2014-06-25 11:20:17	18.35	3.65	239	2014-06-25 11:20:53	79.736	79.844	239	2014-06-25 11:20:34	80.366	78.134
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241	2014-06-25 11:22:17	18.35	3.65	241	2014-06-25 11:22:53	79.754	79.826	241	2014-06-25 11:22:34	80.258	78.422
242	2014-06-25 11:23:17	18.4	3.7	242	2014-06-25 11:23:53	79.736	79.888	242	2014-06-25 11:23:34	80.258	78.638
243	2014-06-25 11:24:17	18.4	3.7	243	2014-06-25 11:24:54	79.718	79.888	243	2014-06-25 11:24:34	80.258	78.904
244	2014-06-25 11:25:17	18.4	3.7	244	2014-06-25 11:25:53	79.718	79.844	244	2014-06-25 11:25:34	80.258	78.904
245	2014-06-25 11:26:17	18.35	3.65	245	2014-06-25 11:26:53	79.736	79.88	245	2014-06-25 11:26:34	80.258	79.124
246	2014-06-25 11:27:17	18.35	3.65	246	2014-06-25 11:27:53	79.772	79.88	246	2014-06-25 11:27:34	80.258	79.25
247	2014-06-25 11:28:17	18.4	3.7	247	2014-06-25 11:28:53	79.772	79.808	247	2014-06-25 11:28:34	80.258	79.394
248	2014-06-25 11:29:17	18.4	3.7	248	2014-06-25 11:29:53	79.736	79.808	248	2014-06-25 11:29:34	80.15	79.476
249	2014-06-25 11:30:17	18.4	3.7	249	2014-06-25 11:30:53	79.718	79.79	249	2014-06-25 11:30:34	80.15	79.448
250	2014-06-25 11:31:17	18.4	3.7	250	2014-06-25 11:31:53	79.736	79.826	250	2014-06-25 11:31:34	80.258	79.61
251	2014-06-25 11:32:17	18.4	3.7	251	2014-06-25 11:32:53	79.79	79.844	251	2014-06-25 11:32:34	80.15	79.538
252	2014-06-25 11:33:17	18.4	3.7	252	2014-06-25 11:33:53	79.79	79.88	252	2014-06-25 11:33:34	80.15	79.592
253	2014-06-25 11:34:17	18.4	3.7	253	2014-06-25 11:34:53	79.736	79.844	253	2014-06-25 11:34:34	80.15	79.628
254	2014-06-25 11:35:17	18.4	3.7	254	2014-06-25 11:35:53	79.79	79.88	254	2014-06-25 11:35:34	80.15	79.628
255	2014-06-25 11:36:17	18.4	3.7	255	2014-06-25 11:36:53	79.718	79.826	255	2014-06-25 11:36:34	80.15	79.682
256	2014-06-25 11:37:17	18.4	3.7	256	2014-06-25 11:37:53	79.808	79.826	256	2014-06-25 11:37:34	80.15	79.718
257	2014-06-25 11:38:17	18.4	3.7	257	2014-06-25 11:38:53	79.736	79.826	257	2014-06-25 11:38:34	80.15	79.772
258	2014-06-25 11:39:17	18.4	3.7	258	2014-06-25 11:39:53	79.79	79.826	258	2014-06-25 11:39:34	80.15	79.772
259	2014-06-25 11:40:17	18.4	3.7	259	2014-06-25 11:40:53	79.772	79.88	259	2014-06-25 11:40:34	80.15	79.808
260	2014-06-25 11:41:17	18.4	3.7	260	2014-06-25 11:41:53	79.808	79.88	260	2014-06-25 11:41:34	80.15	79.844
261	2014-06-25 11:42:17	18.4	3.7	261	2014-06-25 11:42:53	79.772	79.844	261	2014-06-25 11:42:34	80.024	79.718
262	2014-06-25 11:43:17	18.4	3.7	262	2014-06-25 11:43:53	79.772	79.826	262	2014-06-25 11:43:34	80.024	79.718
263	2014-06-25 11:44:17	18.4	3.7	263	2014-06-25 11:44:53	79.772	79.826	263	2014-06-25 11:44:34	80.024	79.718
264	2014-06-25 11:45:17	18.4	3.7	264	2014-06-25 11:45:53	79.736	79.826	264	2014-06-25 11:45:34	80.024	79.988
265	2014-06-25 11:46:17	18.4	3.7	265	2014-06-25 11:46:53	79.772	79.826	265	2014-06-25 11:46:34	80.024	80.024
266	2014-06-25 11:47:17	18.4	3.7	266	2014-06-25 11:47:53	79.772	79.826	266	2014-06-25 11:47:34	80.024	80.024
267	2014-06-25 11:48:17	18.4	3.7	267	2014-06-25 11:48:53	79.736	79.826	267	2014-06-25 11:48:34	80.024	80.024
268	2014-06-25 11:49:17	18.4	3.7	268	2014-06-25 11:49:53	79.718	79.808	268	2014-06-25 11:49:34	80.024	79.952
269	2014-06-25 11:50:17	18.4	3.7	269	2014-06-25 11:50:53	79.826	79.808	269	2014-06-25 11:50:34	80.024	79.898
270	2014-06-25 11:51:17	18.4	3.7	270	2014-06-25 11:51:53	79.754	79.826	270	2014-06-25 11:51:34	80.024	79.718
271	2014-06-25 11:52:17	18.4	3.7	271	2014-06-25 11:52:53	79.772	79.826	271	2014-06-25 11:52:34	80.024	79.322
272	2014-06-25 11:53:17	18.45	3.75	272	2014-06-25 11:53:53	79.772	79.826	272	2014-06-25 11:53:34	80.024	79.286
273	2014-06-25 11:54:17	18.4	3.7	273	2014-06-25 11:54:53	79.736	79.808	273	2014-06-25 11:54:34	80.024	79.016
274	2014-06-25 11:55:17	18.4	3.7	274	2014-06-25 11:55:53	79.772	79.808	274	2014-06-25 11:55:34	80.024	79.106
275	2014-06-25 11:56:17	18.45	3.75	275	2014-06-25 11:56:53	79.772	79.844	275	2014-06-25 11:56:34	80.024	79.286
276	2014-06-25 11:57:17	18.4	3.7	276	2014-06-25 11:57:53	79.736	79.826	276	2014-06-25 11:57:34	80.024	79.376
277	2014-06-25 11:58:17	18.4	3.7	277	2014-06-25 11:58:53	79.718	79.808	277	2014-06-25 11:58:34	80.024	79.466
278	2014-06-25 11:59:17	18.4	3.7	278	2014-06-25 11:59:53	79.772	79.826	278	2014-06-25 11:59:34	80.024	79.556
279	2014-06-25 12:00:17	18.4	3.7	279	2014-06-25 12:00:53	79.736	79.826	279	2014-06-25 12:00:34	80.024	79.592
280	2014-06-25 12:01:17	18.4	3.7	280	2014-06-25 12:01:53	79.808	79.826	280	2014-06-25 12:01:34	80.024	79.646
281	2014-06-25 12:02:17	18.4	3.7	281	2014-06-25 12:02:53	79.736	79.826	281	2014-06-25 12:02:34	80.024	79.682
282	2014-06-25 12:03:17	18.45	3.75	282	2014-06-25 12:03:53	79.808	79.826	282	2014-06-25 12:03:34	80.024	79.682
283	2014-06-25 12:04:17	18.4	3.7	283	2014-06-25 12:04:53	79.772	79.898	283	2014-06-25 12:04:34	80.024	79.718
284	2014-06-25 12:05:17	18.45	3.75	284	2014-06-25 12:05:53	79.772	79.808	284	2014-06-25 12:05:34	80.024	79.718
285	2014-06-25 12:06:17	18.45	3.75	285	2014-06-25 12:06:53	79.772	79.808	285	2014-06-25 12:06:34	80.024	79.718
286	2014-06-25 12:07:17	18.5	3.8	286	2014-06-25 12:07:53	79.772	79.808	286	2014-06-25 12:07:34	80.024	79.772
287	2014-06-25 12:08:17	18.5	3.8	287	2014-06-25 12:08:53	79.736	79.862	287	2014-06-25 12:08:34	80.024	79.952
288	2014-06-25 12:09:17	18.5	3.8	288	2014-06-25 12:09:53	79.808	79.808	288	2014-06-25 12:09:34	80.024	79.952
289	2014-06-25 12:10:17	18.5	3.8	289	2014-06-25 12:10:53	79.754	79.862	289	2014-06-25 12:10:34	79.916	79.844
290	2014-06-25 12:11:17	18.5	3.8	290	2014-06-25 12:11:53	79.754	79.862	290	2014-06-25 12:11:34	80.024	79.898
291	2014-06-25 12:12:17	18.5	3.8	291	2014-06-25 12:12:53	79.808	79.826	291	2014-06-25 12:12:34	80.024	79.898
292	2014-06-25 12:13:17	18.7	4	292	2014-06-25 12:13:53	79.862	79.862	292	2014-06-25 12:13:34	80.024	80.078
293	2014-06-25 12:14:17	22.6	7.8	293	2014-06-25 12:14:53	79.862	79.808	293	2014-06-25 12:14:34	79.916	79.916
294	2014-06-25 12:15:17	19.65	4.95	294	2014-06-25 12:15:53	79.862	79.88	294	2014-06-25 12:15:34	79.916	79.88
295	2014-06-25 12:16:17	18.65	3.95	295	2014-06-25 12:16:53	79.862	79.808	295	2014-06-25 12:16:34	80.024	79.898
296	2014-06-25 12:17:17	18.5	3.8	296	2014-06-25 12:17:53	79.898	79.934	296	2014-06-25 12:17:34	80.024	134.194
297	2014-06-25 12:18:17	16.95	2.25	297	2014-06-25 12:18:53	80.024	79.916	297	2014-06-25 12:18:34	80.024	2498
298	2014-06-25 12:19:17	16.55	1.85	298	2014-06-25 12:19:53	80.024	79.952	298	2014-06-25 12:19:34	80.024	79.718
299	2014-06-25 12:20:17	20.1	5.4	299	2014-06-25 12:20:53	79.952	80.006	299	2014-06-25 12:20:34	80.15	80.078
300	2014-06-25 12:21:17	24.8	10.1	300	2014-06-25 12:21:53	80.024	79.97	300	2014-06-25 12:21:34	80.258	80.348
301	2014-06-25 12:22:17	30.55	15.85	301	2014-06-25 12:22:53	80.024	80.024	301	2014-06-25 12:22:34	80.258	80.006
302	2014-06-25 12:23:17	43.15	28.45	302	2014-06-25 12:23:53	79.988	80.006	302	2014-06-25 12:23:34	80.258	80.186
303	2014-06-25 12:24:17	57.45	42.75	303	2014-06-25 12:24:53	79.97	79.934	303	2014-06-25 12:24:34	80.258	80.258
304	2014-06-25 12:25:17	61.15	46.45	304	2014-06-25 12:25:53	79.97	79.97	304	2014-06-25 12:25:34	80.258	80.042
305	2014-06-25 12:26:17	62.05	47.35	305	2014-06-25 12:26:53	79.97	79.934	305	2014-06-25 12:26:34	80.258	80.006
306	2014-06-25 12:27:17	62.95	48.25	306	2014-06-25 12:27:53	79.934	79.934	306	2014-06-25 12:27:34	80.258	80.132
307	2014-06-25 12:28:17	63.45	48.75	307	2014-06-25 12:28:53	79.97	80.006	307	2014-06-25 12:28:34	80.258	80.222
308	2014-06-25 12:29:17	76.6	61.9	308	2014-06-25 12:29:53	79.898	80.006	308	2014-06-25 12:29:34	80.258	80.758
309	2014-06-25 12:30:17	85.3	69.9	309	2014-06-25 12:30:53	79.898	80.006	309	2014-06-25 12:30:34	80.258	80.348
310	2014-06-25 12:31:17	121.1	117.1	310	2014-06-25 12:31:53	79.934	79.988	310	2014-06-25 12:31:34	80.258	80.258
311	2014-06-25 12:32:17	168.4	153.7	311	2014-06-25 12:32:53	79.988	79.934	311	2014-06-25 12:32:34	80.258	80.312
312	2014-06-25 12:33:17	180.15	165.45	312	2014-06-25 12:33:53	79.952	79.97	312	2014-06-25 12:33:34	80.258	80.258
313	2014-06-25 12:34:17	180	165.3	313	2014-06-25 12:34:53	79.898	79.898	313	2014-06-25 12:34:34	80.258	80.258
314	2014-06-25 12:35:17	179.9	165.2	314	2014-06-25 12:35:53	79.898	79.934	314	2014-06-25 12:35:34	80.258	80.312



332	2014-06-25 12:43:17	179.4	164.7	322	2014-06-25 12:43:53	79.952	80.024	322	2014-06-25 12:43:34	80.258	80.186
333	2014-06-25 12:44:17	180.8	166.1	323	2014-06-25 12:44:53	80.024	79.97	323	2014-06-25 12:44:34	80.258	80.186
334	2014-06-25 12:45:17	180.75	166.05	324	2014-06-25 12:45:53	79.952	80.024	324	2014-06-25 12:45:34	80.258	80.222
335	2014-06-25 12:46:17	180.7	166	325	2014-06-25 12:46:53	79.988	80.006	325	2014-06-25 12:46:34	80.258	80.222
336	2014-06-25 12:47:17	180.65	165.95	326	2014-06-25 12:47:53	79.916	80.078	326	2014-06-25 12:47:34	80.258	80.222
337	2014-06-25 12:48:17	180.6	165.9	327	2014-06-25 12:48:53	79.916	80.06	327	2014-06-25 12:48:34	80.15	80.114
338	2014-06-25 12:49:17	180.55	165.85	328	2014-06-25 12:49:53	79.826	79.952	328	2014-06-25 12:49:34	80.15	80.114
339	2014-06-25 12:50:17	180.55	165.85	329	2014-06-25 12:50:53	79.916	80.006	329	2014-06-25 12:50:34	80.15	80.114
330	2014-06-25 12:51:17	180.5	165.8	330	2014-06-25 12:51:53	79.88	80.006	330	2014-06-25 12:51:34	80.15	80.15
331	2014-06-25 12:52:17	180.45	165.75	331	2014-06-25 12:52:53	79.88	79.952	331	2014-06-25 12:52:34	80.15	80.15
332	2014-06-25 12:53:17	180.45	165.75	332	2014-06-25 12:53:53	79.88	79.916	332	2014-06-25 12:53:34	80.15	80.114
333	2014-06-25 12:54:17	180.4	165.7	333	2014-06-25 12:54:53	79.816	80.006	333	2014-06-25 12:54:34	80.258	80.186
334	2014-06-25 12:55:17	180.35	165.65	334	2014-06-25 12:55:53	79.916	79.97	334	2014-06-25 12:55:34	80.258	80.222
335	2014-06-25 12:56:17	180.3	165.6	335	2014-06-25 12:56:53	79.916	79.916	335	2014-06-25 12:56:34	80.15	80.114
336	2014-06-25 12:57:17	180.3	165.6	336	2014-06-25 12:57:53	79.88	79.97	336	2014-06-25 12:57:34	80.15	80.114
337	2014-06-25 12:58:17	180.25	165.55	337	2014-06-25 12:58:53	79.952	79.952	337	2014-06-25 12:58:34	80.15	80.114
338	2014-06-25 12:59:17	180.2	165.5	338	2014-06-25 12:59:53	80.006	79.916	338	2014-06-25 12:59:34	80.15	80.078
339	2014-06-25 13:00:17	180.2	165.5	339	2014-06-25 13:00:53	80.024	79.916	339	2014-06-25 13:00:34	80.15	80.078
340	2014-06-25 13:01:17	180.15	165.45	340	2014-06-25 13:01:53	80.006	79.916	340	2014-06-25 13:01:34	80.15	80.114
341	2014-06-25 13:02:17	180.15	165.45	341	2014-06-25 13:02:53	80.006	80.006	341	2014-06-25 13:02:34	80.15	80.078
342	2014-06-25 13:03:17	180.1	165.4	342	2014-06-25 13:03:53	80.006	79.898	342	2014-06-25 13:03:34	80.15	80.078
343	2014-06-25 13:04:17	180.05	165.35	343	2014-06-25 13:04:53	80.024	79.916	343	2014-06-25 13:04:34	80.15	80.024
344	2014-06-25 13:05:17	180.05	165.35	344	2014-06-25 13:05:53	80.042	80.024	344	2014-06-25 13:05:34	80.258	80.042
345	2014-06-25 13:06:17	180	165.3	345	2014-06-25 13:06:53	80.06	79.952	345	2014-06-25 13:06:34	80.258	80.042
346	2014-06-25 13:07:17	179.95	165.25	346	2014-06-25 13:07:53	80.06	80.06	346	2014-06-25 13:07:34	80.258	80.042
347	2014-06-25 13:08:17	179.9	165.2	347	2014-06-25 13:08:53	80.042	80.06	347	2014-06-25 13:08:34	80.258	80.006
348	2014-06-25 13:09:17	181.65	166.95	348	2014-06-25 13:09:53	80.06	79.952	348	2014-06-25 13:09:34	80.15	79.898
349	2014-06-25 13:10:17	181.6	166.9	349	2014-06-25 13:10:53	80.06	80.006	349	2014-06-25 13:10:34	80.15	79.944
350	2014-06-25 13:11:17	181.6	166.9	350	2014-06-25 13:11:53	80.006	80.006	350	2014-06-25 13:11:34	80.15	79.988
351	2014-06-25 13:12:17	181.5	166.8	351	2014-06-25 13:12:53	80.06	80.006	351	2014-06-25 13:12:34	80.15	79.988
352	2014-06-25 13:13:17	181.5	166.8	352	2014-06-25 13:13:53	79.988	79.916	352	2014-06-25 13:13:34	80.15	79.988
353	2014-06-25 13:14:17	181.45	166.75	353	2014-06-25 13:14:53	80.06	79.952	353	2014-06-25 13:14:34	80.15	79.988
354	2014-06-25 13:15:17	181.4	166.7	354	2014-06-25 13:15:53	80.042	79.952	354	2014-06-25 13:15:34	80.024	79.862
355	2014-06-25 13:16:17	181.4	166.7	355	2014-06-25 13:16:53	80.006	79.952	355	2014-06-25 13:16:34	80.024	79.862
356	2014-06-25 13:17:17	181.4	166.7	356	2014-06-25 13:17:53	79.952	80.006	356	2014-06-25 13:17:34	80.15	80.024
357	2014-06-25 13:18:17	181.35	166.65	357	2014-06-25 13:18:53	79.952	80.006	357	2014-06-25 13:18:34	80.024	79.862
358	2014-06-25 13:19:17	181.3	166.6	358	2014-06-25 13:19:53	79.916	80.006	358	2014-06-25 13:19:34	80.024	79.898
359	2014-06-25 13:20:17	181.3	166.6	359	2014-06-25 13:20:53	79.916	79.952	359	2014-06-25 13:20:34	80.024	79.862
360	2014-06-25 13:21:17	181.25	166.55	360	2014-06-25 13:21:53	79.88	79.952	360	2014-06-25 13:21:34	80.024	79.898
361	2014-06-25 13:22:17	181.2	166.5	361	2014-06-25 13:22:53	79.97	80.006	361	2014-06-25 13:22:34	80.024	79.898
362	2014-06-25 13:23:17	181.2	166.5	362	2014-06-25 13:23:53	79.916	80.024	362	2014-06-25 13:23:34	80.024	79.862
363	2014-06-25 13:24:17	181.15	166.45	363	2014-06-25 13:24:53	79.952	79.916	363	2014-06-25 13:24:34	80.024	79.898
364	2014-06-25 13:25:17	182.4	167.7	364	2014-06-25 13:25:53	79.898	79.97	364	2014-06-25 13:25:34	80.024	79.862
365	2014-06-25 13:26:17	182.35	167.65	365	2014-06-25 13:26:53	79.88	79.916	365	2014-06-25 13:26:34	80.024	79.898
366	2014-06-25 13:27:17	182.35	167.65	366	2014-06-25 13:27:53	79.916	79.898	366	2014-06-25 13:27:34	80.024	79.952
367	2014-06-25 13:28:17	182.3	167.6	367	2014-06-25 13:28:53	79.916	79.916	367	2014-06-25 13:28:34	80.024	79.898
368	2014-06-25 13:29:17	182.3	167.6	368	2014-06-25 13:29:53	79.862	79.952	368	2014-06-25 13:29:34	80.024	79.952
369	2014-06-25 13:30:17	182.25	167.55	369	2014-06-25 13:30:53	79.898	79.952	369	2014-06-25 13:30:34	80.024	79.898
370	2014-06-25 13:31:17	182.25	167.55	370	2014-06-25 13:31:53	79.88	79.916	370	2014-06-25 13:31:34	79.916	79.79
371	2014-06-25 13:32:17	182.2	167.5	371	2014-06-25 13:32:53	80.006	79.952	371	2014-06-25 13:32:34	80.024	79.898
372	2014-06-25 13:33:17	182.2	167.5	372	2014-06-25 13:33:53	80.006	79.97	372	2014-06-25 13:33:34	80.024	79.862
373	2014-06-25 13:34:17	182.15	167.45	373	2014-06-25 13:34:53	79.952	79.952	373	2014-06-25 13:34:34	80.024	79.862
374	2014-06-25 13:35:17	182.15	167.45	374	2014-06-25 13:35:53	79.988	79.988	374	2014-06-25 13:35:34	80.024	79.898
375	2014-06-25 13:36:17	182.1	167.4	375	2014-06-25 13:36:53	80.006	79.952	375	2014-06-25 13:36:34	80.024	79.862
376	2014-06-25 13:37:17	182.1	167.4	376	2014-06-25 13:37:53	80.042	79.97	376	2014-06-25 13:37:34	80.024	79.862
377	2014-06-25 13:38:17	182.05	167.35	377	2014-06-25 13:38:53	79.988	80.006	377	2014-06-25 13:38:34	80.024	79.898
378	2014-06-25 13:39:17	182	167.3	378	2014-06-25 13:39:53	79.988	80.006	378	2014-06-25 13:39:34	80.024	79.862
379	2014-06-25 13:40:17	182	167.3	379	2014-06-25 13:40:53	80.096	79.97	379	2014-06-25 13:40:34	80.024	79.862
380	2014-06-25 13:41:17	181.95	167.25	380	2014-06-25 13:41:53	80.168	80.024	380	2014-06-25 13:41:34	80.024	79.808
381	2014-06-25 13:42:17	181.95	167.25	381	2014-06-25 13:42:53	80.078	79.952	381	2014-06-25 13:42:34	80.024	79.808
382	2014-06-25 13:43:17	181.95	167.25	382	2014-06-25 13:43:53	80.132	80.024	382	2014-06-25 13:43:34	80.024	79.808
383	2014-06-25 13:44:17	181.9	167.2	383	2014-06-25 13:44:53	80.232	80.06	383	2014-06-25 13:44:34	80.024	79.808
384	2014-06-25 13:45:17	181.85	167.15	384	2014-06-25 13:45:53	80.186	80.024	384	2014-06-25 13:45:34	80.024	79.772
385	2014-06-25 13:46:17	181.85	167.15	385	2014-06-25 13:46:53	80.186	80.024	385	2014-06-25 13:46:34	80.024	79.772
386	2014-06-25 13:47:17	181.8	167.1	386	2014-06-25 13:47:53	80.132	80.024	386	2014-06-25 13:47:34	80.15	79.844
387	2014-06-25 13:48:17	181.8	167.1	387	2014-06-25 13:48:53	80.222	79.97	387	2014-06-25 13:48:34	80.15	79.808
388	2014-06-25 13:49:17	181.75	167.05	388	2014-06-25 13:49:53	80.24	80.06	388	2014-06-25 13:49:34	80.15	79.808
389	2014-06-25 13:50:17	181.75	167.05	389	2014-06-25 13:50:53	80.168	80.024	389	2014-06-25 13:50:34	80.15	79.772
390	2014-06-25 13:51:17	181.7	167	390	2014-06-25 13:51:53	80.168	80.024	390	2014-06-25 13:51:34	80.15	79.718
391	2014-06-25 13:52:17	181.6	166.9	391	2014-06-25 13:52:53	80.168	79.97	391	2014-06-25 13:52:34	80.15	79.718
392	2014-06-25 13:53:17	181.5	166.8	392	2014-06-25 13:53:53	80.132	80.024	392	2014-06-25 13:53:34	80.15	79.718
393	2014-06-25 13:54:17	181.5	166.8	393	2014-06-25 13:54:53	80.132	80.06	393	2014-06-25 13:54:34	80.15	79.718
394	2014-06-25 13:55:17	181.45	166.75	394	2014-06-25 13:55:53	80.096	80.024	394	2014-06-25 13:55:34	80.15	79.682
395	2014-06-25 13:56:17	181.4	166.7	395	2014-06-25 13:56:53	80.042	80.06	395	2014-06-25 13:56:34	80.15	79.718
396	2014-06-25 13:57:17	181.4	166.7	396	2014-06-25 13:57:53	80.024	80.06	396	2014-06-25 13:57:34	80.1	





488	2014-06-25 15:29:17	179	164.3	488	2014-06-25 15:29:53	80.24	80.006	488	2014-06-25 15:29:34	79.916	78.908
489	2014-06-25 15:30:17	178.95	164.25	489	2014-06-25 15:30:53	80.24	80.024	489	2014-06-25 15:30:34	79.916	78.962
490	2014-06-25 15:31:17	178.95	164.25	490	2014-06-25 15:31:53	80.24	80.078	490	2014-06-25 15:31:34	80.024	79.967
491	2014-06-25 15:32:17	178.95	164.25	491	2014-06-25 15:32:53	80.24	80.186	491	2014-06-25 15:32:34	80.024	78.972
492	2014-06-25 15:33:17	178.9	164.2	492	2014-06-25 15:33:53	80.24	80.24	492	2014-06-25 15:33:34	79.916	78.962
493	2014-06-25 15:34:17	178.9	164.2	493	2014-06-25 15:34:53	80.24	80.096	493	2014-06-25 15:34:34	79.916	78.998
494	2014-06-25 15:35:17	178.85	164.15	494	2014-06-25 15:35:53	80.204	80.024	494	2014-06-25 15:35:34	79.916	78.998
495	2014-06-25 15:36:17	178.85	164.15	495	2014-06-25 15:36:53	80.186	80.078	495	2014-06-25 15:36:34	79.916	79.052
496	2014-06-25 15:37:17	178.85	164.15	496	2014-06-25 15:37:53	80.15	80.024	496	2014-06-25 15:37:34	79.916	79.052
497	2014-06-25 15:38:17	178.8	164.1	497	2014-06-25 15:38:53	80.24	80.024	497	2014-06-25 15:38:34	79.916	79.088
498	2014-06-25 15:39:17	178.8	164.1	498	2014-06-25 15:39:53	80.186	80.078	498	2014-06-25 15:39:34	79.916	79.142
499	2014-06-25 15:40:17	178.75	164.05	499	2014-06-25 15:40:53	80.24	80.066	499	2014-06-25 15:40:34	79.916	79.142
500	2014-06-25 15:41:17	178.75	164.05	500	2014-06-25 15:41:53	80.186	80.06	500	2014-06-25 15:41:34	79.916	79.178
501	2014-06-25 15:42:17	178.7	164	501	2014-06-25 15:42:53	80.24	80.024	501	2014-06-25 15:42:34	79.916	79.214
502	2014-06-25 15:43:17	178.7	164	502	2014-06-25 15:43:53	80.15	80.066	502	2014-06-25 15:43:34	79.916	79.268
503	2014-06-25 15:44:17	178.65	163.95	503	2014-06-25 15:44:53	80.186	80.024	503	2014-06-25 15:44:34	79.916	79.304
504	2014-06-25 15:45:17	178.65	163.95	504	2014-06-25 15:45:53	80.132	80.042	504	2014-06-25 15:45:34	79.916	79.268
505	2014-06-25 15:46:17	178.63	163.95	505	2014-06-25 15:46:53	80.294	80.066	505	2014-06-25 15:46:34	79.916	79.304
506	2014-06-25 15:47:17	178.6	163.9	506	2014-06-25 15:47:53	80.186	80.066	506	2014-06-25 15:47:34	79.916	79.358
507	2014-06-25 15:48:17	178.6	163.9	507	2014-06-25 15:48:53	80.24	80.024	507	2014-06-25 15:48:34	79.916	79.358
508	2014-06-25 15:49:17	178.6	163.9	508	2014-06-25 15:49:53	80.204	80.06	508	2014-06-25 15:49:34	79.916	79.358
509	2014-06-25 15:50:17	178.55	163.85	509	2014-06-25 15:50:53	80.15	79.97	509	2014-06-25 15:50:34	79.916	79.358
510	2014-06-25 15:51:17	178.55	163.85	510	2014-06-25 15:51:53	80.114	80.06	510	2014-06-25 15:51:34	80.024	79.412
511	2014-06-25 15:52:17	178.5	163.8	511	2014-06-25 15:52:53	80.132	80.06	511	2014-06-25 15:52:34	79.916	79.214
512	2014-06-25 15:53:17	178.4	163.7	512	2014-06-25 15:53:53	80.15	79.97	512	2014-06-25 15:53:34	80.024	79.376
513	2014-06-25 15:54:17	178.35	163.65	513	2014-06-25 15:54:53	80.15	80.066	513	2014-06-25 15:54:34	80.024	79.412
514	2014-06-25 15:55:17	178.3	163.6	514	2014-06-25 15:55:53	80.15	79.97	514	2014-06-25 15:55:34	80.024	79.376
515	2014-06-25 15:56:17	178.3	163.6	515	2014-06-25 15:56:53	80.15	80.024	515	2014-06-25 15:56:34	80.366	79.412
516	2014-06-25 15:57:17	178.3	163.6	516	2014-06-25 15:57:53	80.186	80.066	516	2014-06-25 15:57:34	80.816	79.466
517	2014-06-25 15:58:17	178.25	163.55	517	2014-06-25 15:58:53	80.186	80.066	517	2014-06-25 15:58:34	81.266	79.358
518	2014-06-25 15:59:17	178.25	163.55	518	2014-06-25 15:59:53	80.24	80.024	518	2014-06-25 15:59:34	81.608	79.466
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521	2014-06-25 16:02:17	182.35	167.65	521	2014-06-25 16:02:53	80.24	79.97	521	2014-06-25 16:02:34	81.5	79.412
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523	2014-06-25 16:04:17	182.3	167.6	523	2014-06-25 16:04:53	80.186	80.024	523	2014-06-25 16:04:34	81.374	79.466
524	2014-06-25 16:05:17	182.3	167.6	524	2014-06-25 16:05:53	80.24	80.024	524	2014-06-25 16:05:34	81.266	79.43
525	2014-06-25 16:06:17	182.25	167.55	525	2014-06-25 16:06:53	80.114	80.024	525	2014-06-25 16:06:34	81.158	79.466
526	2014-06-25 16:07:17	182.25	167.55	526	2014-06-25 16:07:53	80.15	80.024	526	2014-06-25 16:07:34	81.05	79.448
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528	2014-06-25 16:09:17	182.05	167.35	528	2014-06-25 16:09:53	80.114	80.066	528	2014-06-25 16:09:34	80.924	79.484
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534	2014-06-25 16:15:17	181.95	167.25	534	2014-06-25 16:15:53	79.97	79.97	534	2014-06-25 16:15:34	80.6	79.61
535	2014-06-25 16:16:17	181.95	167.25	535	2014-06-25 16:16:53	80.024	80.066	535	2014-06-25 16:16:34	80.474	79.484
536	2014-06-25 16:17:17	181.9	167.2	536	2014-06-25 16:17:53	79.952	79.97	536	2014-06-25 16:17:34	80.474	79.57
537	2014-06-25 16:18:17	181.9	167.2	537	2014-06-25 16:18:53	80.066	79.952	537	2014-06-25 16:18:34	80.474	79.596
538	2014-06-25 16:19:17	181.9	167.2	538	2014-06-25 16:19:53	79.97	80.024	538	2014-06-25 16:19:34	80.474	79.61
539	2014-06-25 16:20:17	181.85	167.15	539	2014-06-25 16:20:53	79.952	80.024	539	2014-06-25 16:20:34	80.366	79.502
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543	2014-06-25 16:24:17	181.75	167.05	543	2014-06-25 16:24:53	79.952	80.06	543	2014-06-25 16:24:34	80.366	79.592
544	2014-06-25 16:25:17	181.75	167.05	544	2014-06-25 16:25:53	80.066	80.024	544	2014-06-25 16:25:34	80.258	79.493
545	2014-06-25 16:26:17	181.7	167	545	2014-06-25 16:26:53	79.952	80.066	545	2014-06-25 16:26:34	80.258	79.52
546	2014-06-25 16:27:17	181.7	167	546	2014-06-25 16:27:53	80.066	79.97	546	2014-06-25 16:27:34	80.258	79.484
547	2014-06-25 16:28:17	181.65	166.95	547	2014-06-25 16:28:53	79.952	79.97	547	2014-06-25 16:28:34	80.258	79.484
548	2014-06-25 16:29:17	181.65	166.95	548	2014-06-25 16:29:53	79.916	79.916	548	2014-06-25 16:29:34	80.258	79.52
549	2014-06-25 16:30:17	181.65	166.95	549	2014-06-25 16:30:53	79.952	80.024	549	2014-06-25 16:30:34	80.258	79.52
550	2014-06-25 16:31:17	181.6	166.9	550	2014-06-25 16:31:53	79.916	79.97	550	2014-06-25 16:31:34	80.258	79.52
551	2014-06-25 16:32:17	181.6	166.9	551	2014-06-25 16:32:53	79.916	80.024	551	2014-06-25 16:32:34	80.258	79.52
552	2014-06-25 16:33:17	181.55	166.85	552	2014-06-25 16:33:53	79.916	80.024	552	2014-06-25 16:33:34	80.258	79.52
553	2014-06-25 16:34:17	181.55	166.85	553	2014-06-25 16:34:53	79.898	79.952	553	2014-06-25 16:34:34	80.258	79.484
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555	2014-06-25 16:36:17	181.5	166.8	555	2014-06-25 16:36:53	79.88	79.898	555	2014-06-25 16:36:34	80.258	79.484
556	2014-06-25 16:37:17	181.5	166.8	556	2014-06-25 16:37:53	79.898	80.066	556	2014-06-25 16:37:34	80.258	79.484
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558	2014-06-25 16:39:17	181.45	166.75	558	2014-06-25 16:39:53	79.88	79.952	558	2014-06-25 16:39:34	80.258	79.484
559	2014-06-25 16:40:17	181.4	166.7	559	2014-06-25 16:40:53	79.88	79.952	559	2014-06-25 16:40:34	80.258	79.484
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561	2014-06-25 16:42:17	181.4	166.7	561	2014-06-25 16:42:53	79.862	79.952	561	2014-06-25 16:42:34	80.258	79.43
562	2014-06-25 16:43:17	181.4	166.7	562	2014-06-25 16:43:53	79.862	79.916	562	2014-06-25 16:43:34	80.25	







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738	2014-06-25 19:39:17	177.75	163.05	738	2014-06-25 19:39:53	79.934	79.88	738	2014-06-25 19:39:34	80.366	80.15
739	2014-06-25 19:40:17	177.7	163.05	739	2014-06-25 19:40:53	79.934	79.88	739	2014-06-25 19:40:34	80.366	80.16
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746	2014-06-25 19:47:17	177.6	162.9	746	2014-06-25 19:47:53	79.934	79.898	746	2014-06-25 19:47:34	80.366	80.15
747	2014-06-25 19:48:17	177.6	162.9	747	2014-06-25 19:48:53	79.988	79.88	747	2014-06-25 19:48:34	80.366	80.15
748	2014-06-25 19:49:17	177.55	162.85	748	2014-06-25 19:49:53	79.934	79.934	748	2014-06-25 19:49:34	80.366	80.14
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752	2014-06-25 19:53:17	177.45	162.75	752	2014-06-25 19:53:53	80.024	79.934	752	2014-06-25 19:53:34	80.258	80.006
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755	2014-06-25 19:56:17	177.4	162.7	755	2014-06-25 19:56:53	79.934	79.952	755	2014-06-25 19:56:34	80.258	80.042
756	2014-06-25 19:57:17	177.4	162.7	756	2014-06-25 19:57:53	79.934	79.88	756	2014-06-25 19:57:34	80.258	80.042
757	2014-06-25 19:58:17	177.35	162.65	757	2014-06-25 19:58:53	79.88	79.934	757	2014-06-25 19:58:34	80.258	80.042
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762	2014-06-25 20:03:17	182.85	168.1	762	2014-06-25 20:03:53	80.042	79.97	762	2014-06-25 20:03:34	80.15	79.898
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765	2014-06-25 20:06:17	182.8	168.1	765	2014-06-25 20:06:53	80.042	79.97	765	2014-06-25 20:06:34	80.15	79.898
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768	2014-06-25 20:09:17	182.75	168.05	768	2014-06-25 20:09:53	79.952	79.97	768	2014-06-25 20:09:34	80.15	79.898
769	2014-06-25 20:10:17	182.75	168.05	769	2014-06-25 20:10:53	79.898	79.952	769	2014-06-25 20:10:34	80.15	79.898
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771	2014-06-25 20:12:17	182.75	168.05	771	2014-06-25 20:12:53	79.916	79.88	771	2014-06-25 20:12:34	80.15	79.898
772	2014-06-25 20:13:17	182.75	168.05	772	2014-06-25 20:13:53	79.916	79.952	772	2014-06-25 20:13:34	80.15	79.898
773	2014-06-25 20:14:17	182.75	168.05	773	2014-06-25 20:14:53	79.862	79.898	773	2014-06-25 20:14:34	80.15	79.934
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775	2014-06-25 20:16:17	182.7	168	775	2014-06-25 20:16:53	79.88	79.898	775	2014-06-25 20:16:34	80.024	79.772
776	2014-06-25 20:17:17	182.7	168	776	2014-06-25 20:17:53	79.88	79.952	776	2014-06-25 20:17:34	80.024	79.718
777	2014-06-25 20:18:17	182.7	168	777	2014-06-25 20:18:53	79.88	79.952	777	2014-06-25 20:18:34	80.024	79.772
778	2014-06-25 20:19:17	182.65	167.95	778	2014-06-25 20:19:53	79.808	79.97	778	2014-06-25 20:19:34	80.024	79.772
779	2014-06-25 20:20:17	182.65	167.95	779	2014-06-25 20:20:53	79.808	79.898	779	2014-06-25 20:20:34	80.024	79.808
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781	2014-06-25 20:22:17	182.6	167.9	781	2014-06-25 20:22:53	79.844	79.952	781	2014-06-25 20:22:34	80.024	79.772
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785	2014-06-25 20:26:17	182.55	167.85	785	2014-06-25 20:26:53	79.844	79.844	785	2014-06-25 20:26:34	80.024	79.772
786	2014-06-25 20:27:17	182.5	167.8	786	2014-06-25 20:27:53	79.808	79.88	786	2014-06-25 20:27:34	80.024	79.808
787	2014-06-25 20:28:17	182.5	167.8	787	2014-06-25 20:28:53	79.826	79.862	787	2014-06-25 20:28:34	80.024	79.772
788	2014-06-25 20:29:17	182.5	167.8	788	2014-06-25 20:29:53	79.826	79.808	788	2014-06-25 20:29:34	80.024	79.718
789	2014-06-25 20:30:17	182.45	167.75	789	2014-06-25 20:30:53	79.79	79.808	789	2014-06-25 20:30:34	80.024	79.718
790	2014-06-25 20:31:17	182.45	167.75	790	2014-06-25 20:31:53	79.844	79.898	790	2014-06-25 20:31:34	80.024	79.772
791	2014-06-25 20:32:17	182.45	167.75	791	2014-06-25 20:32:53	79.826	79.844	791	2014-06-25 20:32:34	80.024	79.772
792	2014-06-25 20:33:17	182.4	167.7	792	2014-06-25 20:33:53	79.88	79.844	792	2014-06-25 20:33:34	79.916	79.664
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794	2014-06-25 20:35:17	182.35	167.65	794	2014-06-25 20:35:53	79.88	79.844	794	2014-06-25 20:35:34	79.916	79.7
795	2014-06-25 20:36:17	182.35	167.65	795	2014-06-25 20:36:53	79.898	79.844	795	2014-06-25 20:36:34	79.916	79.7
796	2014-06-25 20:37:17	182.3	167.6	796	2014-06-25 20:37:53	79.898	79.898	796	2014-06-25 20:37:34	79.916	79.664
797	2014-06-25 20:38:17	182.3	167.6	797	2014-06-25 20:38:53	79.898	79.844	797	2014-06-25 20:38:34	79.916	79.664
798	2014-06-25 20:39:17	182.25	167.55	798	2014-06-25 20:39:53	79.862	79.844	798	2014-06-25 20:39:34	79.916	79.664
799	2014-06-25 20:40:17	182.25	167.55	799	2014-06-25 20:40:53	79.826	79.826	799	2014-06-25 20:40:34	79.916	79.61
800	2014-06-25 20:41:17	182.25	167.55	800	2014-06-25 20:41:53	79.844	79.88	800	2014-06-25 20:41:34	79.916	79.664
801	2014-06-25 20:42:17	182.2	167.5	801	2014-06-25 20:42:53	79.898	79.844	801	2014-06-25 20:42:34	79.916	79.61
802	2014-06-25 20:43:17	182.2	167.5	802	2014-06-25 20:43:53	79.898	79.844	802	2014-06-25 20:43:34	79.916	79.664
803	2014-06-25 20:44:17	182.15	167.45	803	2014-06-25 20:44:53	79.898	79.898	803	2014-06-25 20:44:34	79.916	79.61
804	2014-06-25 20:45:17	182.15	167.45	804	2014-06-25 20:45:53	79.88	79.844	804	2014-06-25 20:45:34	79.916	79.574
805	2014-06-25 20:46:17	182.15	167.45	805	2014-06-25 20:46:53	79.88	79.844	805	2014-06-25 20:46:34	79.916	79.664
806	2014-06-25 20:47:17	182.1	167.4	806	2014-06-25 20:47:53	79.898	79.898	806	2014-06-25 20:47:34	79.916	79.664
807	2014-06-25 20:48:17	182.05	167.35	807	2014-06-25 20:48:53	79.844	79.898	807	2014-06-25 20:48:34	79.916	79.61
808	2014-06-25 20:49:17	182.05	167.35	808	2014-06-25 20:49:53	79.934	79.862	808	2014-06-25 20:49:34	79.916	79.61
809	2014-06-25 20:50:17	182.05	167.35	809	2014-06-25 20:50:53	79.88	79.844	809	2014-06-25 20:50:34	79.916	79.61
810	2014-06-25 20:51:17	182	167.3	810	2014-06-25 20:51:53	79.862	79.88	810	2014-06-25 20:51:34	79.916	79.664
811	2014-06-25 20:52:17	182	167.3	811	2014-06-25 20:52:53	79.898	79.88	811	2014-06-25 20:52:34	79.91	



820	2014-06-25 21:01:17	181.85	167.15	820	2014-06-25 21:01:53	79.516	79.898	820	2014-06-25 21:01:34	79.808	79.592
821	2014-06-25 21:02:17	181.8	167.1	821	2014-06-25 21:02:53	79.534	79.834	821	2014-06-25 21:02:34	79.916	79.7
822	2014-06-25 21:03:17	181.8	167.1	822	2014-06-25 21:03:53	79.516	79.88	822	2014-06-25 21:03:34	79.808	79.592
823	2014-06-25 21:04:17	181.75	167.05	823	2014-06-25 21:04:53	79.898	79.898	823	2014-06-25 21:04:34	79.808	79.592
824	2014-06-25 21:05:17	181.75	167.05	824	2014-06-25 21:05:53	79.88	79.88	824	2014-06-25 21:05:34	79.808	79.592
825	2014-06-25 21:06:17	181.75	167.05	825	2014-06-25 21:06:53	79.862	79.862	825	2014-06-25 21:06:34	79.916	79.754
826	2014-06-25 21:07:17	181.7	167	826	2014-06-25 21:07:53	79.862	79.898	826	2014-06-25 21:07:34	79.916	79.7
827	2014-06-25 21:08:17	181.7	167	827	2014-06-25 21:08:53	79.862	79.844	827	2014-06-25 21:08:34	79.916	79.754
828	2014-06-25 21:09:17	181.65	166.95	828	2014-06-25 21:09:53	79.88	79.898	828	2014-06-25 21:09:34	79.808	79.646
829	2014-06-25 21:10:17	181.65	166.95	829	2014-06-25 21:10:53	79.898	79.898	829	2014-06-25 21:10:34	79.916	79.79
830	2014-06-25 21:11:17	181.65	166.95	830	2014-06-25 21:11:53	79.88	79.844	830	2014-06-25 21:11:34	79.808	79.646
831	2014-06-25 21:12:17	181.6	166.9	831	2014-06-25 21:12:53	79.88	79.88	831	2014-06-25 21:12:34	79.808	79.646
832	2014-06-25 21:13:17	181.6	166.9	832	2014-06-25 21:13:53	79.826	79.88	832	2014-06-25 21:13:34	79.808	79.646
833	2014-06-25 21:14:17	181.55	166.85	833	2014-06-25 21:14:53	79.844	79.952	833	2014-06-25 21:14:34	79.808	79.646
834	2014-06-25 21:15:17	181.55	166.85	834	2014-06-25 21:15:53	79.934	79.98	834	2014-06-25 21:15:34	79.808	79.592
835	2014-06-25 21:16:17	181.5	166.8	835	2014-06-25 21:16:53	79.88	79.898	835	2014-06-25 21:16:34	79.808	79.646
836	2014-06-25 21:17:17	181.5	166.8	836	2014-06-25 21:17:53	79.898	79.844	836	2014-06-25 21:17:34	79.808	79.646
837	2014-06-25 21:18:17	181.5	166.8	837	2014-06-25 21:18:53	79.934	79.898	837	2014-06-25 21:18:34	79.808	79.646
838	2014-06-25 21:19:17	181.45	166.75	838	2014-06-25 21:19:53	79.88	79.898	838	2014-06-25 21:19:34	79.916	79.754
839	2014-06-25 21:20:17	181.45	166.75	839	2014-06-25 21:20:53	79.826	79.844	839	2014-06-25 21:20:34	79.808	79.592
840	2014-06-25 21:21:17	181.4	166.7	840	2014-06-25 21:21:53	79.844	79.898	840	2014-06-25 21:21:34	79.808	79.592
841	2014-06-25 21:22:17	181.4	166.7	841	2014-06-25 21:22:53	79.826	79.898	841	2014-06-25 21:22:34	79.808	79.592
842	2014-06-25 21:23:17	181.4	166.7	842	2014-06-25 21:23:53	79.826	79.844	842	2014-06-25 21:23:34	79.808	79.592
843	2014-06-25 21:24:17	181.35	166.65	843	2014-06-25 21:24:53	79.826	79.826	843	2014-06-25 21:24:34	79.808	79.556
844	2014-06-25 21:25:17	181.35	166.65	844	2014-06-25 21:25:53	79.826	79.844	844	2014-06-25 21:25:34	79.808	79.592
845	2014-06-25 21:26:17	181.35	166.65	845	2014-06-25 21:26:53	79.844	79.844	845	2014-06-25 21:26:34	79.808	79.466
846	2014-06-25 21:27:17	181.3	166.6	846	2014-06-25 21:27:53	79.844	79.844	846	2014-06-25 21:27:34	79.808	79.466
847	2014-06-25 21:28:17	181.3	166.6	847	2014-06-25 21:28:53	79.808	79.844	847	2014-06-25 21:28:34	79.808	79.502
848	2014-06-25 21:29:17	181.3	166.6	848	2014-06-25 21:29:53	79.844	79.826	848	2014-06-25 21:29:34	79.808	79.466
849	2014-06-25 21:30:17	181.25	166.55	849	2014-06-25 21:30:53	79.826	79.898	849	2014-06-25 21:30:34	79.808	79.502
850	2014-06-25 21:31:17	181.25	166.55	850	2014-06-25 21:31:53	79.826	79.898	850	2014-06-25 21:31:34	79.808	79.466
851	2014-06-25 21:32:17	181.25	166.55	851	2014-06-25 21:32:53	79.826	79.88	851	2014-06-25 21:32:34	79.808	79.502
852	2014-06-25 21:33:17	181.2	166.5	852	2014-06-25 21:33:53	79.79	79.844	852	2014-06-25 21:33:34	79.808	79.502
853	2014-06-25 21:34:17	181.2	166.5	853	2014-06-25 21:34:53	79.826	79.898	853	2014-06-25 21:34:34	79.808	79.502
854	2014-06-25 21:35:17	181.15	166.45	854	2014-06-25 21:35:53	79.826	79.88	854	2014-06-25 21:35:34	79.808	79.502
855	2014-06-25 21:36:17	181.15	166.45	855	2014-06-25 21:36:53	79.826	79.934	855	2014-06-25 21:36:34	79.808	79.466
856	2014-06-25 21:37:17	181.15	166.45	856	2014-06-25 21:37:53	79.79	79.88	856	2014-06-25 21:37:34	79.808	79.466
857	2014-06-25 21:38:17	181.1	166.4	857	2014-06-25 21:38:53	79.826	79.898	857	2014-06-25 21:38:34	79.808	79.376
858	2014-06-25 21:39:17	181.1	166.4	858	2014-06-25 21:39:53	79.826	79.844	858	2014-06-25 21:39:34	79.808	79.466
859	2014-06-25 21:40:17	181.05	166.35	859	2014-06-25 21:40:53	79.826	79.934	859	2014-06-25 21:40:34	79.808	79.466
860	2014-06-25 21:41:17	181.05	166.35	860	2014-06-25 21:41:53	79.79	79.898	860	2014-06-25 21:41:34	79.808	79.376
861	2014-06-25 21:42:17	181	166.3	861	2014-06-25 21:42:53	79.826	79.88	861	2014-06-25 21:42:34	79.808	79.376
862	2014-06-25 21:43:17	181	166.3	862	2014-06-25 21:43:53	79.808	79.844	862	2014-06-25 21:43:34	79.808	79.286
863	2014-06-25 21:44:17	180.95	166.25	863	2014-06-25 21:44:53	79.826	79.88	863	2014-06-25 21:44:34	79.808	79.286
864	2014-06-25 21:45:17	180.95	166.25	864	2014-06-25 21:45:53	79.88	79.844	864	2014-06-25 21:45:34	79.808	79.286
865	2014-06-25 21:46:17	180.95	166.25	865	2014-06-25 21:46:53	79.826	79.826	865	2014-06-25 21:46:34	79.808	79.34
866	2014-06-25 21:47:17	180.9	166.2	866	2014-06-25 21:47:53	79.826	79.898	866	2014-06-25 21:47:34	79.808	79.286
867	2014-06-25 21:48:17	180.9	166.2	867	2014-06-25 21:48:53	79.772	79.826	867	2014-06-25 21:48:34	79.808	79.34
868	2014-06-25 21:49:17	180.9	166.2	868	2014-06-25 21:49:53	79.808	79.844	868	2014-06-25 21:49:34	79.808	79.34
869	2014-06-25 21:50:17	180.85	166.15	869	2014-06-25 21:50:53	79.808	79.844	869	2014-06-25 21:50:34	79.808	79.25
870	2014-06-25 21:51:17	180.85	166.15	870	2014-06-25 21:51:53	79.808	79.826	870	2014-06-25 21:51:34	79.808	79.25
871	2014-06-25 21:52:17	180.8	166.1	871	2014-06-25 21:52:53	79.826	79.826	871	2014-06-25 21:52:34	79.808	79.25
872	2014-06-25 21:53:17	180.8	166.1	872	2014-06-25 21:53:53	79.808	79.826	872	2014-06-25 21:53:34	79.808	79.286
873	2014-06-25 21:54:17	180.8	166.1	873	2014-06-25 21:54:53	79.808	79.88	873	2014-06-25 21:54:34	79.808	79.286
874	2014-06-25 21:55:17	180.8	166.1	874	2014-06-25 21:55:53	79.808	79.808	874	2014-06-25 21:55:34	79.808	79.286
875	2014-06-25 21:56:17	180.75	166.05	875	2014-06-25 21:56:53	79.808	79.844	875	2014-06-25 21:56:34	79.808	79.34
876	2014-06-25 21:57:17	180.75	166.05	876	2014-06-25 21:57:53	79.88	79.808	876	2014-06-25 21:57:34	79.808	79.34
877	2014-06-25 21:58:17	180.7	166	877	2014-06-25 21:58:53	79.808	79.898	877	2014-06-25 21:58:34	79.7	79.142
878	2014-06-25 21:59:17	180.7	166	878	2014-06-25 21:59:53	79.88	79.826	878	2014-06-25 21:59:34	79.808	79.286
879	2014-06-25 22:00:17	180.65	165.95	879	2014-06-25 22:00:53	79.79	79.898	879	2014-06-25 22:00:34	79.808	79.34
880	2014-06-25 22:01:17	180.65	165.95	880	2014-06-25 22:01:53	79.79	79.826	880	2014-06-25 22:01:34	79.808	79.34
881	2014-06-25 22:02:17	180.65	165.95	881	2014-06-25 22:02:53	79.754	79.772	881	2014-06-25 22:02:34	79.808	79.34
882	2014-06-25 22:03:17	180.6	165.9	882	2014-06-25 22:03:53	79.808	79.898	882	2014-06-25 22:03:34	79.7	79.142
883	2014-06-25 22:04:17	180.6	165.9	883	2014-06-25 22:04:53	79.772	79.826	883	2014-06-25 22:04:34	79.808	79.286
884	2014-06-25 22:05:17	180.6	165.9	884	2014-06-25 22:05:53	79.808	79.826	884	2014-06-25 22:05:34	79.808	79.34
885	2014-06-25 22:06:17	180.55	165.85	885	2014-06-25 22:06:53	79.772	79.862	885	2014-06-25 22:06:34	79.808	79.34
886	2014-06-25 22:07:17	180.55	165.85	886	2014-06-25 22:07:53	79.826	79.844	886	2014-06-25 22:07:34	79.808	79.34
887	2014-06-25 22:08:17	180.5	165.8	887	2014-06-25 22:08:53	79.826	79.88	887	2014-06-25 22:08:34	79.808	79.376
888	2014-06-25 22:09:17	180.5	165.8	888	2014-06-25 22:09:53	79.88	79.862	888	2014-06-25 22:09:34	79.808	79.376
889	2014-06-25 22:10:17	180.5	165.8	889	2014-06-25 22:10:53	79.808	79.808	889	2014-06-25 22:10:34	79.808	79.376
890	2014-06-25 22:11:17	180.45	165.75	890	2014-06-25 22:11:53	79.826	79.844	890	2014-06-25 22:11:34	79.808	79.376
891	2014-06-25 22:12:17	180.45	165.75	891	2014-06-25 22:12:53	79.808	79.844	891	2014-06-25 22:12:34	79.808	79.34
892	2014-06-25 22:13:17	180.4	165.7	892	2014-06-25 22:13:53	79.808	79.808	892	2014-06-25 22:13:34	79.808	79.34
893	2014-06-25 22:14:17	180.4	165.7	893	2014-06-25 22:14:53	79.808	79.826	893	2014-06-25 22:14:34	79.808	79.34
894	2014-06-25 22:15:17	180.35	165.65	894	2014-06-25 22:15:53	79.772	79.844	894	2014-06-		



903	2014-06-25 22:24:17	180.2	165.5	903	2014-06-25 22:24:53	79.826	79.88	903	2014-06-25 22:24:34	79.808	79.34
904	2014-06-25 22:25:17	180.2	165.5	904	2014-06-25 22:25:53	79.808	79.844	904	2014-06-25 22:25:34	79.808	79.34
905	2014-06-25 22:26:17	180.2	165.5	905	2014-06-25 22:26:53	79.826	79.876	905	2014-06-25 22:26:34	79.808	79.34
906	2014-06-25 22:27:17	180.15	165.45	906	2014-06-25 22:27:53	79.772	79.808	906	2014-06-25 22:27:34	79.808	79.376
907	2014-06-25 22:28:17	180.15	165.45	907	2014-06-25 22:28:53	79.772	79.88	907	2014-06-25 22:28:34	79.808	79.376
908	2014-06-25 22:29:17	180.1	165.4	908	2014-06-25 22:29:53	79.808	79.826	908	2014-06-25 22:29:34	79.808	79.376
909	2014-06-25 22:30:17	180.1	165.4	909	2014-06-25 22:30:53	79.736	79.844	909	2014-06-25 22:30:34	79.808	79.376
910	2014-06-25 22:31:17	180.1	165.4	910	2014-06-25 22:31:53	79.772	79.808	910	2014-06-25 22:31:34	79.808	79.412
911	2014-06-25 22:32:17	180.05	165.35	911	2014-06-25 22:32:53	79.808	79.826	911	2014-06-25 22:32:34	79.808	79.376
912	2014-06-25 22:33:17	180.05	165.35	912	2014-06-25 22:33:53	79.772	79.862	912	2014-06-25 22:33:34	79.7	79.304
913	2014-06-25 22:34:17	180	165.3	913	2014-06-25 22:34:53	79.808	79.826	913	2014-06-25 22:34:34	79.808	79.412
914	2014-06-25 22:35:17	180	165.3	914	2014-06-25 22:35:53	79.736	79.826	914	2014-06-25 22:35:34	79.808	79.34
915	2014-06-25 22:36:17	179.95	165.25	915	2014-06-25 22:36:53	79.844	79.826	915	2014-06-25 22:36:34	79.808	79.376
916	2014-06-25 22:37:17	179.95	165.25	916	2014-06-25 22:37:53	79.808	79.844	916	2014-06-25 22:37:34	79.7	79.268
917	2014-06-25 22:38:17	179.95	165.25	917	2014-06-25 22:38:53	79.79	79.88	917	2014-06-25 22:38:34	79.808	79.376
918	2014-06-25 22:39:17	179.9	165.2	918	2014-06-25 22:39:53	79.772	79.772	918	2014-06-25 22:39:34	79.7	79.268
919	2014-06-25 22:40:17	179.9	165.2	919	2014-06-25 22:40:53	79.808	79.826	919	2014-06-25 22:40:34	79.808	79.376
920	2014-06-25 22:41:17	179.9	165.2	920	2014-06-25 22:41:53	79.772	79.862	920	2014-06-25 22:41:34	79.7	79.268
921	2014-06-25 22:42:17	179.85	165.15	921	2014-06-25 22:42:53	79.808	79.826	921	2014-06-25 22:42:34	79.808	79.376
922	2014-06-25 22:43:17	179.85	165.15	922	2014-06-25 22:43:53	79.754	79.826	922	2014-06-25 22:43:34	79.808	79.412
923	2014-06-25 22:44:17	179.85	165.15	923	2014-06-25 22:44:53	79.772	79.826	923	2014-06-25 22:44:34	79.808	79.376
924	2014-06-25 22:45:17	179.8	165.1	924	2014-06-25 22:45:53	79.772	79.826	924	2014-06-25 22:45:34	79.7	79.232
925	2014-06-25 22:46:17	179.8	165.1	925	2014-06-25 22:46:53	79.718	79.862	925	2014-06-25 22:46:34	79.808	79.376
926	2014-06-25 22:47:17	179.75	165.05	926	2014-06-25 22:47:53	79.772	79.808	926	2014-06-25 22:47:34	79.808	79.412
927	2014-06-25 22:48:17	179.75	165.05	927	2014-06-25 22:48:53	79.754	79.88	927	2014-06-25 22:48:34	79.7	79.304
928	2014-06-25 22:49:17	179.75	165.05	928	2014-06-25 22:49:53	79.754	79.826	928	2014-06-25 22:49:34	79.808	79.412
929	2014-06-25 22:50:17	179.7	165	929	2014-06-25 22:50:53	79.772	79.88	929	2014-06-25 22:50:34	79.808	79.376
930	2014-06-25 22:51:17	179.65	164.95	930	2014-06-25 22:51:53	79.772	79.862	930	2014-06-25 22:51:34	79.808	79.412
931	2014-06-25 22:52:17	179.65	164.95	931	2014-06-25 22:52:53	79.772	79.88	931	2014-06-25 22:52:34	79.808	79.412
932	2014-06-25 22:53:17	179.65	164.95	932	2014-06-25 22:53:53	79.808	79.808	932	2014-06-25 22:53:34	79.7	79.304
933	2014-06-25 22:54:17	179.65	164.95	933	2014-06-25 22:54:53	79.808	79.862	933	2014-06-25 22:54:34	79.7	79.268
934	2014-06-25 22:55:17	179.65	164.95	934	2014-06-25 22:55:53	79.736	79.808	934	2014-06-25 22:55:34	79.7	79.268
935	2014-06-25 22:56:17	179.65	164.95	935	2014-06-25 22:56:53	79.772	79.808	935	2014-06-25 22:56:34	79.7	79.304
936	2014-06-25 22:57:17	179.6	164.9	936	2014-06-25 22:57:53	79.79	79.88	936	2014-06-25 22:57:34	79.7	79.268
937	2014-06-25 22:58:17	179.6	164.9	937	2014-06-25 22:58:53	79.736	79.826	937	2014-06-25 22:58:34	79.808	79.412
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939	2014-06-25 23:00:17	179.55	164.85	939	2014-06-25 23:00:53	79.844	79.772	939	2014-06-25 23:00:34	79.808	79.412
940	2014-06-25 23:01:17	179.5	164.8	940	2014-06-25 23:01:53	79.772	79.826	940	2014-06-25 23:01:34	79.808	79.466
941	2014-06-25 23:02:17	179.5	164.8	941	2014-06-25 23:02:53	79.772	79.862	941	2014-06-25 23:02:34	79.7	79.304
942	2014-06-25 23:03:17	179.5	164.8	942	2014-06-25 23:03:53	79.772	79.808	942	2014-06-25 23:03:34	79.808	79.412
943	2014-06-25 23:04:17	179.45	164.75	943	2014-06-25 23:04:53	79.772	79.808	943	2014-06-25 23:04:34	79.7	79.304
944	2014-06-25 23:05:17	179.45	164.75	944	2014-06-25 23:05:53	79.772	79.772	944	2014-06-25 23:05:34	79.808	79.412
945	2014-06-25 23:06:17	179.4	164.7	945	2014-06-25 23:06:53	79.826	79.772	945	2014-06-25 23:06:34	79.808	79.412
946	2014-06-25 23:07:17	179.4	164.7	946	2014-06-25 23:07:53	79.754	79.772	946	2014-06-25 23:07:34	79.7	79.304
947	2014-06-25 23:08:17	179.4	164.7	947	2014-06-25 23:08:53	79.754	79.808	947	2014-06-25 23:08:34	79.808	79.412
948	2014-06-25 23:09:17	179.35	164.65	948	2014-06-25 23:09:53	79.754	79.862	948	2014-06-25 23:09:34	79.7	79.304
949	2014-06-25 23:10:17	179.35	164.65	949	2014-06-25 23:10:53	79.772	79.772	949	2014-06-25 23:10:34	79.808	79.466
950	2014-06-25 23:11:17	179.35	164.65	950	2014-06-25 23:11:53	79.772	79.808	950	2014-06-25 23:11:34	79.808	79.466
951	2014-06-25 23:12:17	179.3	164.6	951	2014-06-25 23:12:53	79.772	79.826	951	2014-06-25 23:12:34	79.808	79.412
952	2014-06-25 23:13:17	179.3	164.6	952	2014-06-25 23:13:53	79.826	79.826	952	2014-06-25 23:13:34	79.7	79.304
953	2014-06-25 23:14:17	179.25	164.55	953	2014-06-25 23:14:53	79.772	79.808	953	2014-06-25 23:14:34	79.7	79.304
954	2014-06-25 23:15:17	179.25	164.55	954	2014-06-25 23:15:53	79.754	79.808	954	2014-06-25 23:15:34	79.7	79.304
955	2014-06-25 23:16:17	179.2	164.5	955	2014-06-25 23:16:53	79.772	79.772	955	2014-06-25 23:16:34	79.808	79.412
956	2014-06-25 23:17:17	179.2	164.5	956	2014-06-25 23:17:53	79.754	79.754	956	2014-06-25 23:17:34	79.7	79.304
957	2014-06-25 23:18:17	179.2	164.5	957	2014-06-25 23:18:53	79.754	79.772	957	2014-06-25 23:18:34	79.7	79.304
958	2014-06-25 23:19:17	179.15	164.45	958	2014-06-25 23:19:53	79.772	79.826	958	2014-06-25 23:19:34	79.7	79.304
959	2014-06-25 23:20:17	179.15	164.45	959	2014-06-25 23:20:53	79.754	79.826	959	2014-06-25 23:20:34	79.808	79.466
960	2014-06-25 23:21:17	179.1	164.4	960	2014-06-25 23:21:53	79.808	79.826	960	2014-06-25 23:21:34	79.7	79.304
961	2014-06-25 23:22:17	179.1	164.4	961	2014-06-25 23:22:53	79.754	79.772	961	2014-06-25 23:22:34	79.808	79.466
962	2014-06-25 23:23:17	179.1	164.4	962	2014-06-25 23:23:53	79.754	79.862	962	2014-06-25 23:23:34	79.7	79.304
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964	2014-06-25 23:25:17	179.05	164.35	964	2014-06-25 23:25:53	79.736	79.772	964	2014-06-25 23:25:34	79.7	79.358
965	2014-06-25 23:26:17	179.05	164.35	965	2014-06-25 23:26:53	79.772	79.88	965	2014-06-25 23:26:34	79.808	79.466
966	2014-06-25 23:27:17	179.05	164.35	966	2014-06-25 23:27:53	79.826	79.772	966	2014-06-25 23:27:34	79.7	79.304
967	2014-06-25 23:28:17	179.05	164.35	967	2014-06-25 23:28:53	79.772	79.88	967	2014-06-25 23:28:34	79.7	79.358
968	2014-06-25 23:29:17	179	164.3	968	2014-06-25 23:29:53	79.808	79.772	968	2014-06-25 23:29:34	79.7	79.358
969	2014-06-25 23:30:17	179	164.3	969	2014-06-25 23:30:53	79.772	79.862	969	2014-06-25 23:30:34	79.7	79.358
970	2014-06-25 23:31:17	178.95	164.25	970	2014-06-25 23:31:53	79.754	79.772	970	2014-06-25 23:31:34	79.7	79.358
971	2014-06-25 23:32:17	178.95	164.25	971	2014-06-25 23:32:53	79.754	79.862	971	2014-06-25 23:32:34	79.7	79.358
972	2014-06-25 23:33:17	178.95	164.25	972	2014-06-25 23:33:53	79.772	79.826	972	2014-06-25 23:33:34	79.7	79.358
973	2014-06-25 23:34:17	178.9	164.2	973	2014-06-25 23:34:53	79.772	79.772	973	2014-06-25 23:34:34	79.7	79.358
974	2014-06-25 23:35:17	178.9	164.2	974	2014-06-25 23:35:53	79.772	79.862	974	2014-06-25 23:35:34	79.808	79.466
975	2014-06-25 23:36:17	178.85	164.15	975	2014-06-25 23:36:53	79.772	79.772	975	2014-06-25 23:36:34	79.7	79.358
976	2014-06-25 23:37:17	178.85	164.15	976	2014-06-25 23:37:53	79.754	79.808	976	2014-06-25 23:37:34	79.7	79.358
977	2014-06-25 23:38:17	178.8	164.1	977	2014-06-25 23:38:53	79.808	79.826	977	2014-06-25 23:38:34	79.7	



986	2014-06-25 23:47:17	178.65	163.95	986	2014-06-25 23:47:53	79.808	79.772	986	2014-06-25 23:47:34	79.7	79.394
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988	2014-06-25 23:49:17	178.6	163.9	988	2014-06-25 23:49:53	79.754	79.808	988	2014-06-25 23:49:34	79.7	79.394
989	2014-06-25 23:50:17	178.6	163.9	989	2014-06-25 23:50:53	79.754	79.808	989	2014-06-25 23:50:34	79.7	79.394
990	2014-06-25 23:51:17	178.6	163.9	990	2014-06-25 23:51:53	79.808	79.826	990	2014-06-25 23:51:34	79.7	79.394
991	2014-06-25 23:52:17	178.55	163.85	991	2014-06-25 23:52:53	79.772	79.862	991	2014-06-25 23:52:34	79.7	79.394
992	2014-06-25 23:53:17	178.55	163.85	992	2014-06-25 23:53:53	79.772	79.808	992	2014-06-25 23:53:34	79.7	79.394
993	2014-06-25 23:54:17	178.55	163.85	993	2014-06-25 23:54:53	79.7	79.826	993	2014-06-25 23:54:34	79.7	79.394
994	2014-06-25 23:55:17	178.5	163.8	994	2014-06-25 23:55:53	79.772	79.808	994	2014-06-25 23:55:34	79.7	79.394
995	2014-06-25 23:56:17	178.5	163.8	995	2014-06-25 23:56:53	79.754	79.826	995	2014-06-25 23:56:34	79.7	79.394
996	2014-06-25 23:57:17	178.45	163.75	996	2014-06-25 23:57:53	79.754	79.772	996	2014-06-25 23:57:34	79.7	79.394
997	2014-06-25 23:58:17	178.45	163.75	997	2014-06-25 23:58:53	79.772	79.754	997	2014-06-25 23:58:34	79.7	79.394
998	2014-06-25 23:59:17	178.45	163.75	998	2014-06-25 23:59:53	79.772	79.862	998	2014-06-25 23:59:34	79.7	79.358
999	2014-06-26 00:00:17	178.45	163.75	999	2014-06-26 00:00:53	79.754	79.754	999	2014-06-26 00:00:34	79.7	79.358
1000	2014-06-26 00:01:17	178.4	163.7	1000	2014-06-26 00:01:53	79.808	79.826	1000	2014-06-26 00:01:34	79.7	79.394
1001	2014-06-26 00:02:17	178.4	163.7	1001	2014-06-26 00:02:53	79.754	79.826	1001	2014-06-26 00:02:34	79.7	79.394
1002	2014-06-26 00:03:17	178.4	163.7	1002	2014-06-26 00:03:53	79.772	79.754	1002	2014-06-26 00:03:34	79.7	79.358
1003	2014-06-26 00:04:17	178.35	163.65	1003	2014-06-26 00:04:53	79.718	79.826	1003	2014-06-26 00:04:34	79.7	79.394
1004	2014-06-26 00:05:17	178.35	163.65	1004	2014-06-26 00:05:53	79.808	79.898	1004	2014-06-26 00:05:34	79.7	79.394
1005	2014-06-26 00:06:17	178.3	163.6	1005	2014-06-26 00:06:53	79.808	79.772	1005	2014-06-26 00:06:34	79.7	79.394
1006	2014-06-26 00:07:17	178.3	163.6	1006	2014-06-26 00:07:53	79.88	79.826	1006	2014-06-26 00:07:34	79.7	79.394
1007	2014-06-26 00:08:17	178.3	163.6	1007	2014-06-26 00:08:53	79.754	79.772	1007	2014-06-26 00:08:34	79.7	79.394
1008	2014-06-26 00:09:17	178.25	163.55	1008	2014-06-26 00:09:53	79.826	79.826	1008	2014-06-26 00:09:34	79.7	79.394
1009	2014-06-26 00:10:17	178.25	163.55	1009	2014-06-26 00:10:53	79.754	79.808	1009	2014-06-26 00:10:34	79.7	79.394
1010	2014-06-26 00:11:17	178.25	163.55	1010	2014-06-26 00:11:53	79.754	79.808	1010	2014-06-26 00:11:34	79.7	79.394
1011	2014-06-26 00:12:17	178.2	163.5	1011	2014-06-26 00:12:53	79.754	79.772	1011	2014-06-26 00:12:34	79.7	79.448
1012	2014-06-26 00:13:17	178.2	163.5	1012	2014-06-26 00:13:53	79.772	79.808	1012	2014-06-26 00:13:34	79.7	79.394
1013	2014-06-26 00:14:17	178.2	163.5	1013	2014-06-26 00:14:53	79.772	79.862	1013	2014-06-26 00:14:34	79.7	79.394
1014	2014-06-26 00:15:17	178.15	163.45	1014	2014-06-26 00:15:53	79.754	79.862	1014	2014-06-26 00:15:34	79.7	79.394
1015	2014-06-26 00:16:17	178.15	163.45	1015	2014-06-26 00:16:53	79.772	79.772	1015	2014-06-26 00:16:34	79.7	79.394
1016	2014-06-26 00:17:17	178.1	163.4	1016	2014-06-26 00:17:53	79.808	79.772	1016	2014-06-26 00:17:34	79.7	79.448
1017	2014-06-26 00:18:17	178.1	163.4	1017	2014-06-26 00:18:53	79.754	79.772	1017	2014-06-26 00:18:34	79.7	79.394
1018	2014-06-26 00:19:17	178.05	163.35	1018	2014-06-26 00:19:53	79.754	79.862	1018	2014-06-26 00:19:34	79.7	79.394
1019	2014-06-26 00:20:17	178.05	163.35	1019	2014-06-26 00:20:53	79.736	79.808	1019	2014-06-26 00:20:34	79.7	79.394
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1021	2014-06-26 00:22:17	178.05	163.35	1021	2014-06-26 00:22:53	79.754	79.772	1021	2014-06-26 00:22:34	79.808	79.502
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1024	2014-06-26 00:25:17	177.95	163.25	1024	2014-06-26 00:25:53	79.718	79.772	1024	2014-06-26 00:25:34	79.7	79.448
1025	2014-06-26 00:26:17	177.95	163.25	1025	2014-06-26 00:26:53	79.772	79.808	1025	2014-06-26 00:26:34	79.7	79.394
1026	2014-06-26 00:27:17	177.9	163.2	1026	2014-06-26 00:27:53	79.754	79.772	1026	2014-06-26 00:27:34	79.7	79.394
1027	2014-06-26 00:28:17	177.9	163.2	1027	2014-06-26 00:28:53	79.718	79.772	1027	2014-06-26 00:28:34	79.574	79.322
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1029	2014-06-26 00:30:17	177.85	163.15	1029	2014-06-26 00:30:53	79.718	79.772	1029	2014-06-26 00:30:34	79.7	79.394
1030	2014-06-26 00:31:17	177.85	163.15	1030	2014-06-26 00:31:53	79.754	79.862	1030	2014-06-26 00:31:34	79.7	79.448
1031	2014-06-26 00:32:17	177.85	163.15	1031	2014-06-26 00:32:53	79.754	79.808	1031	2014-06-26 00:32:34	79.7	79.448
1032	2014-06-26 00:33:17	177.85	163.15	1032	2014-06-26 00:33:53	79.772	79.772	1032	2014-06-26 00:33:34	79.7	79.448
1033	2014-06-26 00:34:17	177.8	163.1	1033	2014-06-26 00:34:53	79.772	79.772	1033	2014-06-26 00:34:34	79.7	79.448
1034	2014-06-26 00:35:17	177.8	163.1	1034	2014-06-26 00:35:53	79.808	79.808	1034	2014-06-26 00:35:34	79.574	79.268
1035	2014-06-26 00:36:17	177.8	163.1	1035	2014-06-26 00:36:53	79.718	79.826	1035	2014-06-26 00:36:34	79.7	79.448
1036	2014-06-26 00:37:17	177.75	163.05	1036	2014-06-26 00:37:53	79.754	79.826	1036	2014-06-26 00:37:34	79.7	79.448
1037	2014-06-26 00:38:17	177.75	163.05	1037	2014-06-26 00:38:53	79.808	79.826	1037	2014-06-26 00:38:34	79.7	79.448
1038	2014-06-26 00:39:17	177.75	163.05	1038	2014-06-26 00:39:53	79.754	79.754	1038	2014-06-26 00:39:34	79.7	79.394
1039	2014-06-26 00:40:17	177.75	163.05	1039	2014-06-26 00:40:53	79.808	79.826	1039	2014-06-26 00:40:34	79.7	79.448
1040	2014-06-26 00:41:17	177.7	163	1040	2014-06-26 00:41:53	79.772	79.826	1040	2014-06-26 00:41:34	79.7	79.448
1041	2014-06-26 00:42:17	177.7	163	1041	2014-06-26 00:42:53	79.754	79.754	1041	2014-06-26 00:42:34	79.7	79.394
1042	2014-06-26 00:43:17	177.7	163	1042	2014-06-26 00:43:53	79.718	79.772	1042	2014-06-26 00:43:34	79.7	79.448
1043	2014-06-26 00:44:17	177.65	162.95	1043	2014-06-26 00:44:53	79.754	79.772	1043	2014-06-26 00:44:34	79.7	79.448
1044	2014-06-26 00:45:17	177.65	162.95	1044	2014-06-26 00:45:53	79.754	79.826	1044	2014-06-26 00:45:34	79.7	79.394
1045	2014-06-26 00:46:17	177.6	162.9	1045	2014-06-26 00:46:53	79.754	79.808	1045	2014-06-26 00:46:34	79.7	79.448
1046	2014-06-26 00:47:17	177.6	162.9	1046	2014-06-26 00:47:53	79.718	79.826	1046	2014-06-26 00:47:34	79.7	79.448
1047	2014-06-26 00:48:17	177.55	162.85	1047	2014-06-26 00:48:53	79.754	79.772	1047	2014-06-26 00:48:34	79.7	79.448
1048	2014-06-26 00:49:17	177.55	162.85	1048	2014-06-26 00:49:53	79.808	79.808	1048	2014-06-26 00:49:34	79.7	79.448
1049	2014-06-26 00:50:17	177.55	162.85	1049	2014-06-26 00:50:53	79.754	79.862	1049	2014-06-26 00:50:34	79.7	79.448
1050	2014-06-26 00:51:17	177.5	162.8	1050	2014-06-26 00:51:53	79.718	79.772	1050	2014-06-26 00:51:34	79.7	79.448
1051	2014-06-26 00:52:17	177.5	162.8	1051	2014-06-26 00:52:53	79.826	79.716	1051	2014-06-26 00:52:34	79.7	79.448
1052	2014-06-26 00:53:17	177.45	162.75	1052	2014-06-26 00:53:53	79.772	79.808	1052	2014-06-26 00:53:34	79.7	79.448
1053	2014-06-26 00:54:17	177.45	162.75	1053	2014-06-26 00:54:53	79.754	79.772	1053	2014-06-26 00:54:34	79.7	79.448
1054	2014-06-26 00:55:17	177.45	162.75	1054	2014-06-26 00:55:53	79.772	79.772	1054	2014-06-26 00:55:34	79.7	79.448
1055	2014-06-26 00:56:17	177.4	162.7	1055	2014-06-26 00:56:53	79.754	79.754	1055	2014-06-26 00:56:34	79.7	79.394
1056	2014-06-26 00:57:17	177.4	162.7	1056	2014-06-26 00:57:53	79.736	79.772	1056	2014-06-26 00:57:34	79.7	79.448
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1058	2014-06-26 00:59:17	177.35	162.65	1058	2014-06-26 00:59:53	79.754	79.754	1058	2014-06-26 00:59:34	79.7	79.448
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1080	2014-06-26 01:21:17	177	162.3	1080	2014-06-26 01:21:53	79.682	79.718	1080	2014-06-26 01:21:34	79.7	79.448
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1090	2014-06-26 01:31:17	176.8	162.1	1090	2014-06-26 01:31:53	79.7	79.808	1090	2014-06-26 01:31:34	79.7	79.448
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1092	2014-06-26 01:33:17	176.75	162.05	1092	2014-06-26 01:33:53	79.754	79.754	1092	2014-06-26 01:33:34	79.574	79.358
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1098	2014-06-26 01:39:17	176.65	161.95	1098	2014-06-26 01:39:53	79.736	79.808	1098	2014-06-26 01:39:34	79.7	79.448
1099	2014-06-26 01:40:17	176.65	161.95	1099	2014-06-26 01:40:53	79.718	79.754	1099	2014-06-26 01:40:34	79.7	79.448
1100	2014-06-26 01:41:17	176.65	161.95	1100	2014-06-26 01:41:53	79.682	79.718	1100	2014-06-26 01:41:34	79.7	79.448
1101	2014-06-26 01:42:17	176.65	161.95	1101	2014-06-26 01:42:53	79.718	79.754	1101	2014-06-26 01:42:34	79.7	79.448
1102	2014-06-26 01:43:17	176.6	161.9	1102	2014-06-26 01:43:53	79.682	79.718	1102	2014-06-26 01:43:34	79.7	79.448
1103	2014-06-26 01:44:17	176.6	161.9	1103	2014-06-26 01:44:53	79.7	79.7	1103	2014-06-26 01:44:34	79.7	79.448
1104	2014-06-26 01:45:17	176.6	161.9	1104	2014-06-26 01:45:53	79.718	79.772	1104	2014-06-26 01:45:34	79.7	79.448
1105	2014-06-26 01:46:17	176.55	161.85	1105	2014-06-26 01:46:53	79.682	79.808	1105	2014-06-26 01:46:34	79.7	79.448
1106	2014-06-26 01:47:17	176.55	161.85	1106	2014-06-26 01:47:53	79.754	79.754	1106	2014-06-26 01:47:34	79.7	79.448
1107	2014-06-26 01:48:17	176.5	161.8	1107	2014-06-26 01:48:53	79.682	79.718	1107	2014-06-26 01:48:34	79.574	79.358
1108	2014-06-26 01:49:17	176.5	161.8	1108	2014-06-26 01:49:53	79.7	79.718	1108	2014-06-26 01:49:34	79.7	79.448
1109	2014-06-26 01:50:17	176.5	161.8	1109	2014-06-26 01:50:53	79.664	79.664	1109	2014-06-26 01:50:34	79.7	79.448
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1111	2014-06-26 01:52:17	176.45	161.75	1111	2014-06-26 01:52:53	79.718	79.772	1111	2014-06-26 01:52:34	79.7	79.448
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1115	2014-06-26 01:56:17	176.35	161.65	1115	2014-06-26 01:56:53	79.646	79.754	1115	2014-06-26 01:56:34	79.7	79.448
1116	2014-06-26 01:57:17	176.35	161.65	1116	2014-06-26 01:57:53	79.7	79.772	1116	2014-06-26 01:57:34	79.7	79.448
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1122	2014-06-26 02:03:17	176.25	161.55	1122	2014-06-26 02:03:53	79.736	79.718	1122	2014-06-26 02:03:34	79.7	79.538
1123	2014-06-26 02:04:17	176.25	161.55	1123	2014-06-26 02:04:53	79.646	79.718	1123	2014-06-26 02:04:34	79.7	79.448
1124	2014-06-26 02:05:17	176.25	161.55	1124	2014-06-26 02:05:53	79.682	79.718	1124	2014-06-26 02:05:34	79.7	79.448
1125	2014-06-26 02:06:17	176.2	161.5	1125	2014-06-26 02:06:53	79.646	79.754	1125	2014-06-26 02:06:34	79.7	79.448
1126	2014-06-26 02:07:17	176.2	161.5	1126	2014-06-26 02:07:53	79.718	79.754	1126	2014-06-26 02:07:34	79.7	79.538
1127	2014-06-26 02:08:17	176.15	161.45	1127	2014-06-26 02:08:53	79.7	79.718	1127	2014-06-26 02:08:34	79.7	79.538
1128	2014-06-26 02:09:17	176.15	161.45	1128	2014-06-26 02:09:53	79.646	79.754	1128	2014-06-26 02:09:34	79.7	79.538
1129	2014-06-26 02:10:17	176.15	161.45	1129	2014-06-26 02:10:53	79.7	79.772	1129	2014-06-26 02:10:34	79.7	79.448
1130	2014-06-26 02:11:17	176.1	161.4	1130	2014-06-26 02:11:53	79.646	79.736	1130	2014-06-26 02:11:34	79.7	79.448
1131	2014-06-26 02:12:17	176.1	161.4	1131	2014-06-26 02:12:53	79.682	79.754	1131	2014-06-26 02:12:34	79.7	79.448
1132	2014-06-26 02:13:17	176.05	161.35	1132	2014-06-26 02:13:53	79.718	79.7	1132	2014-06-26 02:13:34	79.7	79.448
1133	2014-06-26 02:14:17	176.05	161.35	1133	2014-06-26 02:14:53	79.718	79.718	1133	2014-06-26 02:14:34	79.7	79.538
1134	2014-06-26 02:15:17	176.05	161.35	1134	2014-06-26 02:15:53	79.682	79.718	1134	2014-06-26 02:15:34	79.574	79.412
1135	2014-06-26 02:16:17	176	161.35	1135	2014-06-26 02:16:53	79.682	79.754	1135	2014-06-26 02:16:34	79.574	79.412
1136	2014-06-26 02:17:17	176	161.3	1136	2014-06-26 02:17:53	79.664	79.754	1136	2014-06-26 02:17:34	79.7	79.538
1137	2014-06-26 02:18:17	176	161.3	1137	2014-06-26 02:18:53	79.718	79.718	1137	2014-06-26 02:18:34	79.7	79.448
1138	2014-06-26 02:19:17	176	161.3	1138	2014-06-26 02:19:53	79.736	79.736	1138	2014-06-26 02:19:34	79.574	79.412
1139	2014-06-26 02:20:17	175.95	161.25	1139	2014-06-26 02:20:53	79.7	79.718	1139	2014-06-26 02:20:34	79.7	79.448
1140	2014-06-26 02:21:17	175.95	161.25	1140	2014-06-26 02:21:53	79.754	79.772	1140	2014-06-26 02:21:34	79.7	79.448
1141	2014-06-26 02:22:17	175.9	161.2	1141	2014-06-26 02:22:53	79.7	79.754	1141	2014-06-26 02:22:34	79.7	79.538
1142	2014-06-26 02:23:17	175.9	161.2	1142	2014-06-26 02:23:53	79.682	79.754	1142	2014-06-26 02:23:34	79.574	79.358
1143	2014-0										



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1153	2014-06-26 02:34:17	175.7	161	1153	2014-06-26 02:34:53	79.754	79.754	1153	2014-06-26 02:34:34	79.7	79.538
1154	2014-06-26 02:35:17	175.7	161	1154	2014-06-26 02:35:53	79.7	79.736	1154	2014-06-26 02:35:34	79.7	79.538
1155	2014-06-26 02:36:17	175.7	161	1155	2014-06-26 02:36:53	79.682	79.718	1155	2014-06-26 02:36:34	79.7	79.538
1156	2014-06-26 02:37:17	175.65	160.95	1156	2014-06-26 02:37:53	79.754	79.682	1156	2014-06-26 02:37:34	79.7	79.538
1157	2014-06-26 02:38:17	175.65	160.95	1157	2014-06-26 02:38:53	79.79	79.754	1157	2014-06-26 02:38:34	79.7	79.538
1158	2014-06-26 02:39:17	175.6	160.9	1158	2014-06-26 02:39:53	79.816	79.7	1158	2014-06-26 02:39:34	79.7	79.484
1159	2014-06-26 02:40:17	175.6	160.9	1159	2014-06-26 02:40:53	79.771	79.7	1159	2014-06-26 02:40:34	79.7	79.538
1160	2014-06-26 02:41:17	175.6	160.9	1160	2014-06-26 02:41:53	79.7	79.7	1160	2014-06-26 02:41:34	79.7	79.538
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1162	2014-06-26 02:43:17	175.55	160.85	1162	2014-06-26 02:43:53	79.736	79.826	1162	2014-06-26 02:43:34	79.7	79.538
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1164	2014-06-26 02:45:17	175.5	160.8	1164	2014-06-26 02:45:53	79.772	79.7	1164	2014-06-26 02:45:34	79.574	79.412
1165	2014-06-26 02:46:17	175.5	160.8	1165	2014-06-26 02:46:53	79.754	79.772	1165	2014-06-26 02:46:34	79.7	79.538
1166	2014-06-26 02:47:17	175.5	160.8	1166	2014-06-26 02:47:53	79.754	79.772	1166	2014-06-26 02:47:34	79.7	79.538
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1172	2014-06-26 02:53:17	175.4	160.7	1172	2014-06-26 02:53:53	79.754	79.718	1172	2014-06-26 02:53:34	79.7	79.538
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1174	2014-06-26 02:55:17	175.35	160.65	1174	2014-06-26 02:55:53	79.682	79.718	1174	2014-06-26 02:55:34	79.7	79.538
1175	2014-06-26 02:56:17	175.35	160.65	1175	2014-06-26 02:56:53	79.808	79.718	1175	2014-06-26 02:56:34	79.7	79.538
1176	2014-06-26 02:57:17	175.35	160.65	1176	2014-06-26 02:57:53	79.682	79.772	1176	2014-06-26 02:57:34	79.7	79.574
1177	2014-06-26 02:58:17	175.3	160.6	1177	2014-06-26 02:58:53	79.718	79.754	1177	2014-06-26 02:58:34	79.7	79.574
1178	2014-06-26 02:59:17	175.3	160.6	1178	2014-06-26 02:59:53	79.7	79.7	1178	2014-06-26 02:59:34	79.7	79.538
1179	2014-06-26 03:00:17	175.3	160.6	1179	2014-06-26 03:00:53	79.772	79.718	1179	2014-06-26 03:00:34	79.7	79.538
1180	2014-06-26 03:01:17	175.25	160.5	1180	2014-06-26 03:01:53	79.754	79.808	1180	2014-06-26 03:01:34	79.7	79.538
1181	2014-06-26 03:02:17	175.25	160.5	1181	2014-06-26 03:02:53	79.718	79.718	1181	2014-06-26 03:02:34	79.574	79.412
1182	2014-06-26 03:03:17	175.25	160.55	1182	2014-06-26 03:03:53	79.754	79.718	1182	2014-06-26 03:03:34	79.7	79.538
1183	2014-06-26 03:04:17	175.2	160.5	1183	2014-06-26 03:04:53	79.7	79.754	1183	2014-06-26 03:04:34	79.7	79.538
1184	2014-06-26 03:05:17	175.2	160.5	1184	2014-06-26 03:05:53	79.772	79.754	1184	2014-06-26 03:05:34	79.7	79.538
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1186	2014-06-26 03:07:17	175.15	160.45	1186	2014-06-26 03:07:53	79.754	79.718	1186	2014-06-26 03:07:34	79.574	79.412
1187	2014-06-26 03:08:17	175.15	160.45	1187	2014-06-26 03:08:53	79.7	79.718	1187	2014-06-26 03:08:34	79.7	79.538
1188	2014-06-26 03:09:17	175.1	160.4	1188	2014-06-26 03:09:53	79.754	79.718	1188	2014-06-26 03:09:34	79.7	79.538
1189	2014-06-26 03:10:17	175.1	160.4	1189	2014-06-26 03:10:53	79.7	79.826	1189	2014-06-26 03:10:34	79.7	79.574
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1191	2014-06-26 03:12:17	175.05	160.35	1191	2014-06-26 03:12:53	79.808	79.772	1191	2014-06-26 03:12:34	79.574	79.484
1192	2014-06-26 03:13:17	175.05	160.35	1192	2014-06-26 03:13:53	79.7	79.754	1192	2014-06-26 03:13:34	79.7	79.538
1193	2014-06-26 03:14:17	175	160.3	1193	2014-06-26 03:14:53	79.736	79.754	1193	2014-06-26 03:14:34	79.7	79.574
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1387	2014-06-26 06:28:17	171.85	157.15	1387	2014-06-26 06:28:53	79.754	79.754	1387	2014-06-26 06:28:34	79.7	79.574
1388	2014-06-26 06:29:17	171.8	157.1	1388	2014-06-26 06:29:53	79.718	79.754	1388	2014-06-26 06:29:34	79.7	79.574
1389	2014-06-26 06:30:17	171.85	157.15	1389	2014-06-26 06:30:53	79.718	79.754	1389	2014-06-26 06:30:34	79.7	79.574
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1543	2014-06-26 09:04:17	169.7	155	1543	2014-06-26 09:04:53	79.808	79.898	1543	2014-06-26 09:04:34	79.7	79.61
1544	2014-06-26 09:05:17	169.65	154.95	1544	2014-06-26 09:05:53	79.79	79.88	1544	2014-06-26 09:05:34	79.7	79.61
1545	2014-06-26 09:06:17	169.65	154.95	1545	2014-06-26 09:06:53	79.79	79.844	1545	2014-06-26 09:06:34	79.7	79.61
1546	2014-06-26 09:07:17	169.6	154.9	1546	2014-06-26 09:07:53	79.826	79.898	1546	2014-06-26 09:07:34	79.7	79.61
1547	2014-06-26 09:08:17	169.6	154.9	1547	2014-06-26 09:08:53	79.844	79.88	1547	2014-06-26 09:08:34	79.7	79.61
1548	2014-06-26 09:09:17	169.6	154.9	1548	2014-06-26 09:09:53	79.736	79.844	1548	2014-06-26 09:09:34	79.7	79.61
1549	2014-06-26 09:10:17	169.55	154.85	1549	2014-06-26 09:10:53	79.826	79.808	1549	2014-06-26 09:10:34	79.7	79.61
1550	2014-06-26 09:11:17	169.5	154.8	1550	2014-06-26 09:11:53	79.844	79.862	1550	2014-06-26 09:11:34	79.7	79.61
1551	2014-06-26 09:12:17	169.45	154.75	1551	2014-06-26 09:12:53	79.736	79.826	1551	2014-06-26 09:12:34	79.7	79.61
1552	2014-06-26 09:13:17	169.4	154.7	1552	2014-06-26 09:13:53	79.88	79.826	1552	2014-06-26 09:13:34	79.7	79.61
1553	2014-06-26 09:14:17	184.15	169.45	1553	2014-06-26 09:14:53	79.898	79.844	1553	2014-06-26 09:14:34	79.7	79.61
1554	2014-06-26 09:15:17	19.2	4.5	1554	2014-06-26 09:15:53	79.988	79.826	1554	2014-06-26 09:15:34	79.7	79.61
1555	2014-06-26 09:16:17	14.7	0	1555	2014-06-26 09:16:53	80.006	79.844	1555	2014-06-26 09:16:34	79.7	79.61
1556	2014-06-26 09:17:17	15.05	0.35	1556	2014-06-26 09:17:53	79.988	79.844	1556	2014-06-26 09:17:34	79.7	79.61
1557	2014-06-26 09:18:17	15.05	0.35	1557	2014-06-26 09:18:53	80.004	79.88	1557	2014-06-26 09:18:34	79.7	79.61
1558	2014-06-26 09:19:17	15.1	0.4	1558	2014-06-26 09:19:53</						





PIPELINE PETROLEUM SERVICES, INC.

Tank 5 - Line Pressure Testing Report  
Red Hill Fuel Farm, Oahu, HI

**APPENDIX E –**

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**INSTRUMENT CALIBRATION CERTIFICATES**

**Certificate Information**

Certificate Number: NC-14-04-11-001  
 Calibration Technician: James Day  
 Calibration Date: 2014-04-11  
 Next Calibration Due: 2015-04-11

**Device Information**

Device Name: PR2000-500psi  
 Device ID: Unit 1 Press  
 Serial Number: N84154  
 Model Description: Pressure Data Logger with Display

MadgeTech, Inc. certifies that the instrument identified below has been calibrated (except where otherwise noted) using calibration standards that are traceable to the National Institute of Standards and Technology (NIST). This certificate is copyrighted and may not be reproduced, except in full, without prior written approval of MadgeTech, Inc..

PR2000-500psi

- Pressure (absolute) -

Serial Number: N84154

The Pressure (absolute) channel of the device under test (DUT) was calibrated in direct comparison to the reference equipment listed on the last page of this calibration certificate.

**Published Device Specifications**

Calibrated Accuracy: ±10.00 psi  
 Calibrated Accuracy Range: 5 psi to 500 psi  
 Resolution: 0.05 psi  
 Notes:

**Channel 1 - Units of psi**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device - Standard	Device Allowable Limits = Standard ± Accuracy	DUT Corrected Device As Left	Device Error = Device - Standard
1	14.750	14.75	0.00	4.75 to 24.75	14.75	0.00
2	400.000	399.95	-0.05	390.00 to 410.00	400.00	0.00

**Initial Correction Values**
**Applied Correction Values**

Gain: 0.9928412      0.9926453  
 Offset: -3.36535 psi      -3.3610001 psi

**Maintaining Calibration:**

This product is manufactured from the highest quality components. The unit has been designed to remain within its specifications during normal use. However, the length of in-tolerance service can be affected by low battery voltage, age, temperature, humidity, shock, and other environmental influences. For those users with critical performance or validation requirements, MadgeTech, Inc. recommends that the unit be serviced and calibrated at regular periodic intervals.

Reference Equipment	Serial #	Certificate #	Last Calibration Date	Next Calibration Due
Mensor CPC6000	611758	96293 / 96304	2013-12-13	2014-12-13

Certificate Number: NC-14-04-11-001  
 Date Created: 2014-04-11  
 Date Printed: 2014-04-11  
 Template Revision: General-11  
 Certificate Page: Page 1 of 2

Company: MadgeTech, Inc.  
 Contact: 6 Warner Road  
 Information: Warner NH  
 03278 USA

www.madgetech.com  
 info@madgetech.com  
 1-603-456-2012  
 1-603-456-2011



**Calibration and Service:**

---

For information regarding this calibration or to arrange factory calibration or other service for this product, contact MadgeTech, Inc. or an authorized reseller. Products shipped directly to MadgeTech, Inc. will require a Return Merchandise Authorization (RMA) number.

**Calibration Notes:**

---

Issued By:	<i>J. Day</i>	Date:	2014-04-11
Approved By:	<i>K. Strese</i>	Date:	2014-04-11

---

Certificate Number: NC-14-04-11-001  
Date Created: 2014-04-11  
Date Printed: 2014-04-11  
Template Revision: General-11  
Certificate Page: Page 2 of 2

Company: MadgeTech, Inc.  
Contact: 6 Warner Road  
Information: Warner NH  
03278 USA

www.madgetech.com  
info@madgetech.com  
1-603-456-2012  
1-603-456-2011



# CERTIFICATE OF CALIBRATION

### Certificate Information:

Certificate Number: AR-13-08-20-003  
 Calibration Technician: J Day  
 Calibration Date: 8/20/2013  
 Next Calibration Due: 8/20/2014

### Device Information:

Device Name: TCTemp2000  
 Device ID: Aux Temp & Unit |  
 Serial Number: N84147  
 Model Description: Thermocouple Temperature Recorder  
 Calibration Date As Received: 7/18/2012  
 Condition As Received: Used  
 Condition As Left: In Tolerance

MadgeTech, Inc. certifies that the instrument identified below has been calibrated using calibration standards that are traceable to the National Institute of Standards and Technology (NIST). This certificate is copyrighted and may not be reproduced, except in full, without prior written approval of MadgeTech, Inc.

### TCTemp2000 -Temperature Channel- Serial Number: N84147

The Temperature channel of the device under test (DUT) was calibrated in direct comparison to the reference equipment listed on the last page of this calibration certificate.

### Published Device Specifications

Accuracy:  $\pm 0.5^{\circ}\text{C}$   
 Range: 0 to  $+50^{\circ}\text{C}$   
 Resolution: 0.01

#### Channel 1 - All data is in degrees Celsius ( $^{\circ}\text{C}$ )

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard $\pm$ Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	25	24.76	-0.24	24.5 to 25.5	25	0

	Initial Correction Values	Applied Correction Values
Gain:	1	1
Offset:	0.12	-0.12

### TCTemp2000 -T/C Channel- Serial Number: N84147

#### Channel 2 - All data is in Millivolts (mV)

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard $\pm$ Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	0	-0.000064	0	N/A	0	0

	Initial Correction	Applied Correction Values
Gain:	1	1
Offset:	-0.000086	-0.00015000001

### Maintaining Calibration:

This product is manufactured from the highest quality components. The unit has been designed to remain within its specifications during normal use. However, the length of in-tolerance service can be affected by low battery voltage, age, temperature, humidity, shock, and other environmental influences. For those users with critical performance or validation requirements, MadgeTech, Inc. recommends that the unit be serviced and calibrated at regular periodic intervals.

### Calibration And Service:

For information regarding this calibration, or to arrange factory calibration or other service for this product, contact MadgeTech or an authorized reseller. Products shipped directly to MadgeTech, Inc. will require a Return Material Authorization (RMA) number.

Certificate Number: AR-13-08-20-003  
 Date Created: 8/20/2013  
 Date Printed: 8/20/2013  
 Certificate Page: Page 1

Company: MadgeTech  
 Contact: 6 Warner Road  
 Information: Warner NH, 03278

(603) 456-2011 (Tel)  
 (603) 456-2012 (Fax)  
 info@madgetech.com (E)  
 http://www.madgetech.com (W)





# CERTIFICATE OF CALIBRATION

Issued By: J. Day

Date: 8/20/2013

Approved By: J. Heald

Date: 8/20/2013

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Reference Equipment	Serial No	Certificate No	Last Cal Date	Next Cal Due
Rotronic HygroClip IC1 Thermo-Hygrometer	43142019	2013.30047	4/30/2013	4/13/2014

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Certificate Number: AR-13-08-20-003  
Date Created: 8/20/2013  
Date Printed: 8/20/2013  
Certificate Page: Page 2

Company: MadgeTech  
Contact: 6 Warner Road  
Information: Warner NH 03278

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info@madgetech.com (E)  
<http://www.madgetech.com> (W)





# CERTIFICATE OF CALIBRATION

**Certificate Information:**

Certificate Number: AR-13-08-21-001  
 Calibration Technician: J Day  
 Calibration Date: 8/21/2013  
 Next Calibration Due: 8/21/2014

**Device Information:**

Device Name: QuadTemp2000  
 Device ID: Temp Unit 1  
 Serial Number: N82430  
 Model Description: Four Channel Thermocouple Recorder  
 Calibration Date As Received: 7/16/2012  
 Condition As Received: Used  
 Condition As Left: In Tolerance

MadgeTech, Inc. certifies that the instrument identified below has been calibrated using calibration standards that are traceable to the National Institute of Standards and Technology (NIST). This certificate is copyrighted and may not be reproduced, except in full, without prior written approval of MadgeTech, Inc.

**QuadTemp2000 -Temperature Channel- Serial Number: N82430**

The Temperature channels of the device under test (DUT) were calibrated in direct comparison to the reference equipment listed on the last page of this calibration certificate.

**Published Device Specifications**

Accuracy:  $\pm 0.5^{\circ}\text{C}$   
 Range: 0 to  $+ 50^{\circ}\text{C}$   
 Resolution: 0.01

**Channel 1 - All data is in degrees Celsius ( $^{\circ}\text{C}$ )**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard $\pm$ Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	25	24.79	-0.21	24.5 to 25.5	24.99	-0.01
2	60	60.35	0.35	59.5 to 60.5	60.02	0.02
		<b>Initial Correction Values</b>	<b>Applied Correction Values</b>			
Gain:	1.0008	1.0168571				
Offset:	1.350008	0.73857141				

**Channel 3 - All data is in degrees Celsius ( $^{\circ}\text{C}$ )**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard $\pm$ Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	25	24.71	-0.29	24.5 to 25.5	25	0
2	60	60.32	0.32	59.5 to 60.5	60.02	0.02
		<b>Initial Correction Values</b>	<b>Applied Correction Values</b>			
Gain:	1.0024	1.0197144				
Offset:	-2.2799759	-3.0028572				

**Channel 5 - All data is in degrees Celsius ( $^{\circ}\text{C}$ )**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard $\pm$ Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	25	24.65	-0.35	24.5 to 25.5	25.01	0.01
2	60	60.27	0.27	59.5 to 60.5	59.99	-0.01
		<b>Initial Correction Values</b>	<b>Applied Correction Values</b>			
Gain:	1	1.0177143				
Offset:	0.81	0.017142856				

**Channel 7 - All data is in degrees Celsius ( $^{\circ}\text{C}$ )**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard $\pm$ Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	25	24.52	-0.48	24.5 to 25.5	24.99	-0.01
2	60	60.15	0.15	59.5 to 60.5	60	0
		<b>Initial Correction Values</b>	<b>Applied Correction Values</b>			
Gain:	0.98839998	1.006				

Certificate Number: AR-13-08-21-001  
 Date Created: 8/21/2013  
 Date Printed: 8/21/2013  
 Certificate Page: Page 1

Company: MadgeTech  
 Contact: 6 Warner Road  
 Information: Warner NH 03278

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 http://www.madgetech.com (W)





# CERTIFICATE OF CALIBRATION

Offset: 0.079884 -0.82999998

QuadTemp2000 -T/C Channel- Serial Number: N82430

**Channel 2 - All data is in Millivolts (mV)**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard±Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	0	-0.000326	0	N/A	0	0
Initial Correction		Applied Correction Values				
Gain:	1	1				
Offset:	-0.00050700002	-0.000833				

**Channel 4 - All data is in Millivolts (mV)**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard±Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	0	0.000212	0	N/A	0	0
Initial Correction		Applied Correction Values				
Gain:	1	1				
Offset:	-0.000439	-0.000227				

**Channel 6 - All data is in Millivolts (mV)**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard±Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	0	-0.000108	0	N/A	0	0
Initial Correction		Applied Correction Values				
Gain:	1	1				
Offset:	-0.000799999998	-0.000907999999				

**Channel 8 - All data is in Millivolts (mV)**

Point	Standard Actual Test Point	DUT Uncorrected Device As Found	Device Error = Device-Standard	Allowable Device Limits = Standard±Accuracy	DUT Corrected Device As Left	Device Error = Device-Standard
1	0	-0.000165	0	N/A	0	0
Initial Correction		Applied Correction Values				
Gain:	1	1				
Offset:	0.000014	-0.000151				

**Maintaining Calibration:**

This product is manufactured from the highest quality components. The unit has been designed to remain within its specifications during normal use. However, the length of in-tolerance service can be affected by low battery voltage, age, temperature, humidity, shock, and other environmental influences. For those users with critical performance or validation requirements, MadgeTech, Inc. recommends that the unit be serviced and calibrated at regular periodic intervals.

**Calibration And Service:**

For information regarding this calibration, or to arrange factory calibration or other service for this product, contact MadgeTech or an authorized reseller. Products shipped directly to MadgeTech, Inc. will require a Return Material Authorization (RMA) number.

Issued By:

*J. Day*

Date:

8/21/2013

Approved By:

*J. Heald*

Date:

8/21/2013

Certificate Number: AR-13-08-21-001  
 Date Created: 8/21/2013  
 Date Printed: 8/21/2013  
 Certificate Page: Page 2

Company: MadgeTech  
 Contact: 6 Warner Road  
 Information: Warner NH 03278

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 http://www.madgetech.com (W)



**AI Angel's  
INC. Instrumentation  
ISO 17025 ACCREDITED**

**CERTIFICATE OF CALIBRATION**

Angel's Instrumentation Inc.  
928 Canal Drive  
Chesapeake, VA 23323

UNIT UNDER TEST(UUT): 10 GPM Flow Meter  
MANUFACTURER: GPI  
MODEL NUMBER: G2S05N09GMA  
SERIAL NUMBER: 3206877  
CUSTOMER ID NUMBER: 211871 **UNIT 3**  
PROCEDURE NAME: 17-20MG-38 (Rev. 8/1/2010)  
CALIBRATED BY: Dante Daneri  
CONTACT NAME: Dennis Cobb  
CUSTOMER: Pipeline Petroleum Service  
1324 Cavalier Blvd  
CHESAPEAKE, VA 23323

TEST RESULT: PASS  
PERFORMED ON: 6/16/2014  
TEMPERATURE: 22.4°C  
HUMIDITY: 46%  
CAL DATE: 6/16/2014  
NEXT CAL DUE: 6/16/2015  
WORKORDER#: 25137  
CERTIFICATE#: 211871:6856481481  
Purchase Order#: Verbal Dennis  
DATA TYPE: FOUND-LEFT  
PERFORMED AT Angel's Instrumentation Inc.

Angel's Instrumentation Inc. certifies that the above listed instrument meets or exceeds all specifications as stated in the referenced procedure unless otherwise noted. It has been calibrated using measurement standards traceable to the National Institute of Standards and Technology (NIST), to NIST accepted intrinsic standards of measurement, or derived by the ratio type of self-calibration techniques. This calibration complies with ISO-IEC 17025-2005, ANSI/NCSL Z540-1-1994, and/or ANSI/NCSL Z540.3-2006.

Complete records of work performed are maintained by Angel's Instrumentation and are available for inspection. All calibrations have been performed using processes that have a test uncertainty ratio of four or more times greater than the unit calibrated. Uncertainties have been estimated at 95 percent confidence level (k=2). Calibration at 4:1 TUR provides reasonable confidence that the instrument is within the manufacturer's published specifications.

This report may not be reproduced, except in full, unless permission for the publication of an approved abstract is obtained in writing from the calibration organization issuing this report.

Note: Any Test Uncertainty Ratio (TUR) that is less than four to one will appear in the remarks section of this report and identified with an asterisk (\*) in the readings section.

Note: Any number of factors may cause the calibration item to drift out of calibration before the recommended interval has expired. The customer is responsible for assigning intervals. Angel's Instrumentation does not recommend calibration intervals.

Angel's Instrumentation is responsible for the calibration process results during the time of the calibration process, and this certificate of calibration is neither a contract nor a contractual representation.

REMARKS: Received on 6/16/2014.

Received Condition: Fair / In Tolerance

**Standards Used**

Asset	Description	CAL DUE DATE
300018	Flow Meter	28-May-16

REPORT OF CALIBRATION for SERIAL NUMBER: 3206877 CUSTOMER ID: 211871  
PRINTED ON: 16-Jun-14 GPI G2S05N09GMA \*211871\*



**Test Data**

Flow Calibration

Range	Applied	As Found	As Left	Lower Limit	Upper Limit	
10 GPM	2 GPM	1.99	1.99	1.96	2.04	PASS
.	4 GPM	3.99	3.99	3.92	4.08	PASS
.	6 GPM	5.99	5.99	5.88	6.12	PASS
.	8 GPM	7.99	7.99	7.84	8.16	PASS

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**End of Test Data**

Signed:



Authorized Service Technician/Manager

Signed:



Designated Service QA Manager



# A/I Angel's INC. Instrumentation ISO 17025 ACCREDITED

## CERTIFICATE OF CALIBRATION

Angel's Instrumentation Inc.  
928 Canal Drive  
Chesapeake, VA 23323

UNIT UNDER TEST(UUT): 5-50 GPM Flow Meter MANUFACTURER: GPI MODEL NUMBER: G2S10N09GMA SERIAL NUMBER: 3710745 CUSTOMER ID NUMBER: 211872 <i>UNIT 4 - 1" φ</i> PROCEDURE NAME: 17-20MG-38 (Rev. 8/1/2014) CALIBRATED BY: Dante Daneri CONTACT NAME: Dennis Cobb CUSTOMER: Pipeline Petroleum Service 1324 Cavalier Blvd CHESAPEAKE, VA 23323	TEST RESULT: PASS PERFORMED ON: 6/16/2014 TEMPERATURE: 22.4°C HUMIDITY: 46% CAL DATE: 6/16/2014 NEXT CAL DUE: 6/16/2015 WORKORDER#: 25137 CERTIFICATE#: 211872:6885416667 Purchase Order#: Verbal Dennis DATA TYPE: FOUND-LEFT PERFORMED AT Angel's Instrumentation Inc.
--	--

Angel's Instrumentation Inc. certifies that the above listed instrument meets or exceeds all specifications as stated in the referenced procedure unless otherwise noted. It has been calibrated using measurement standards traceable to the National Institute of Standards and Technology (NIST), to NIST accepted intrinsic standards of measurement, or derived by the ratio type of self-calibration techniques. This calibration complies with ISO-IEC 17025-2005, ANSI/NCSL Z540-1-1994, and/or ANSI/NCSL Z540.3-2006.

Complete records of work performed are maintained by Angel's Instrumentation and are available for inspection. All calibrations have been performed using processes that have a test uncertainty ratio of four or more times greater than the unit calibrated. Uncertainties have been estimated at 95 percent confidence level (k=2). Calibration at 4:1 TUR provides reasonable confidence that the instrument is within the manufacturer's published specifications.

This report may not be reproduced, except in full, unless permission for the publication of an approved abstract is obtained in writing from the calibration organization issuing this report.

Note: Any Test Uncertainty Ratio (TUR) that is less than four to one will appear in the remarks section of this report and identified with an asterisk (\*) in the readings section.

Note: Any number of factors may cause the calibration item to drift out of calibration before the recommended interval has expired. The customer is responsible for assigning intervals. Angel's Instrumentation does not recommend calibration intervals.

Angel's Instrumentation is responsible for the calibration process results during the time of the calibration process, and this certificate of calibration is neither a contract nor a contractual representation.

REMARKS: Received on 6/16/2014.

Received Condition: Fair / In Tolerance

### Standards Used

Asset	Description	CAL DUE DATE
300018	Flow Meter	28-May-16

REPORT OF CALIBRATION for SERIAL NUMBER: 3710745 CUSTOMER ID: 211872  
 PRINTED ON: 16-Jun-14 GPI G2S10N09GMA \*211872\*



## Test Data

### Flow Calibration

Range	Applied	As Found	As Left	Lower Limit	Upper Limit	
5 GPM	10 GPM	9.95	9.95	9.85	10.15	PASS
.	20 GPM	19.96	19.96	19.70	20.30	PASS
.	30 GPM	29.95	29.95	29.55	30.45	PASS
30 GPM	40 GPM	39.94	39.94	39.40	40.60	PASS

## End of Test Data

Signed:



Authorized Service Technician/Manager

Signed:



Designated Service QA Manager

REPORT OF CALIBRATION for SERIAL NUMBER: 3710745 CUSTOMER ID: 211872

PRINTED ON: 16-Jun-14 GPI G2S10N09GMA

\*211872\*



# Angel's Instrumentation INC. ISO 17025 ACCREDITED

## CERTIFICATE OF CALIBRATION

Angel's Instrumentation Inc.  
928 Canal Drive  
Chesapeake, VA 23323

<p>UNIT UNDER TEST(UUT): 5000 PSI Pressure Gauge          MANUFACTURER: Crystal Engineering          MODEL NUMBER: XP21 5000          SERIAL NUMBER: 870422          CUSTOMER ID NUMBER: 211596 <i>UNIT 1</i>          PROCEDURE NAME: AILCP-136 (Rev. 2)          CALIBRATED BY: Dante Daneri          CONTACT NAME: Joe Jackson          CUSTOMER: Pipeline Petroleum Service          1324 Cavalier Blvd          CHESAPEAKE, VA 23323</p>	<p>TEST RESULT: PASS          PERFORMED ON: 5/5/2014          TEMPERATURE: 20.2°C          HUMIDITY: 47%          CAL DATE: 5/5/2014          NEXT CAL DUE: 5/5/2015          WORKORDER#: 24846          CERTIFICATE#: 211596.6267592593          Purchase Order#: CHARGE          DATA TYPE: FOUND-LEFT          PERFORMED AT Angel's Instrumentation Inc.</p>
---	---

Angel's Instrumentation Inc. certifies that the above listed instrument meets or exceeds all specifications as stated in the referenced procedure unless otherwise noted. It has been calibrated using measurement standards traceable to the National Institute of Standards and Technology (NIST), to NIST accepted intrinsic standards of measurement, or derived by the ratio type of self-calibration techniques. This calibration complies with ISO-IEC 17025-2005, ANSI/NC SL Z540-1-1994, and/or ANSI/NC SL Z540.3-2006.

Complete records of work performed are maintained by Angel's Instrumentation and are available for inspection. All calibrations have been performed using processes that have a test uncertainty ratio of four or more times greater than the unit calibrated. Uncertainties have been estimated at 95 percent confidence level (k=2). Calibration at 4:1 TUR provides reasonable confidence that the instrument is within the manufacturer's published specifications.

This report may not be reproduced, except in full, unless permission for the publication of an approved abstract is obtained in writing from the calibration organization issuing this report.

Note: Any Test Uncertainty Ratio (TUR) that is less than four to one will appear in the remarks section of this report and identified with an asterisk (\*) in the readings section.

Note: Any number of factors may cause the calibration item to drift out of calibration before the recommended interval has expired. The customer is responsible for assigning intervals. Angel's Instrumentation does not recommend calibration intervals.

Angel's Instrumentation is responsible for the calibration process results during the time of the calibration process, and this certificate of calibration is neither a contract nor a contractual representation.

REMARKS: Received on 5/5/2014.

Received Condition: Good / In Tolerance

### Standards Used

Asset	Description	CAL DUE DATE
301068	RTD Probe w/ Indicator	16-Dec-15
301069	100 Kg Mass Set	04-Oct-14
301071	500 PSI Piston	10-Sep-14

REPORT OF CALIBRATION for SERIAL NUMBER: 870422 CUSTOMER ID: 211596  
 PRINTED ON: 05-May-14 Crystal Engineering XP21 5000 \*211596\*



## Test Data

### Digital Pressure Calibration

DUT

Set Point	Applied	As Found	As Left	Lower Limit	Upper Limit	
500 PSI	499.797	500.0	500.0	498.80	500.80	Pass
1000 PSI	999.845	1000.0	1000.0	998.85	1000.85	Pass
1500 PSI	1499.893	1500.0	1500.0	1498.39	1501.39	Pass
2000 PSI	1999.937	1999.8	1999.8	1997.94	2001.94	Pass
2500 PSI	2499.983	2499.5	2499.5	2497.48	2502.48	Pass
3000 PSI	3000.027	2999.5	2999.5	2997.03	3003.03	Pass
3500 PSI	3500.063	3499.5	3499.5	3496.56	3503.56	Pass
4000 PSI	4000.098	3999.5	3999.5	3996.10	4004.10	Pass
4500 PSI	4500.128	4499.4	4499.4	4495.63	4504.63	Pass
5000 PSI	5000.162	4999.6	4999.6	4995.16	5005.16	Pass

Device Under Test Accuracy +/- .02% F.S. from 0-20% of F.S. and +/- .1% Rdg from 20-100% of F.S.

## End of Test Data

Signed:

  
Authorized Service Technician/Manager

Signed:

  
Designated Service QA Manager

REPORT OF CALIBRATION for SERIAL NUMBER: 870422

CUSTOMER ID: 211596

PRINTED ON: 05-May-14 Crystal Engineering XP2i 5000

\*211596\*



**QUALITY ASSURANCE SURVEILLANCE PLAN**

**WARRANTY PHASE WORK  
RE-INSPECT AND REPAIR RED HILL TANK 5  
JBPHH, Pearl Harbor, HI  
Contract Number N62583-09-D-0132/0003**

Issued 13 Nov 2014

**FOR CONSTRUCTION**

Rev Number	Date	Comment
8	6 Nov 2014	Incorporated SME comments to draft matrix in Attachment 6; PAC and NFHI comments incorporated; QAI role added



## TABLE OF CONTENTS

1	INTRODUCTION .....	1
1.1	Purpose.....	1
1.2	Performance Management Approach.....	1
1.3	Performance Management Strategy .....	2
2	ROLES AND RESPONSIBILITIES .....	3
2.1	The Contracting Officer .....	3
2.2	The Contracting Officer’s Representative.....	3
2.3	The Project Manager .....	3
2.4	Construction Surveillance Engineer .....	3
2.5	Construction Surveillance Engineering Technician .....	4
2.6	Quality Assurance Inspector .....	4
3	METHODOLOGIES TO MONITOR PERFORMANCE .....	4
3.1	Proactive Surveillance Techniques .....	4
3.2	Participatory Surveillance Techniques .....	5
3.3	Customer Feedback.....	6
3.4	Acceptable Quality Levels .....	7
4	QUALITY ASSURANCE DOCUMENTATION .....	7
4.1	The Performance Management Feedback Loop.....	7
4.2	Quality Assurance Reports.....	7
5	ANALYSIS OF QUALITY ASSURANCE ASSESSMENT .....	7
5.1	Determining Performance .....	7
5.2	Reporting.....	8
5.3	Reviews and Resolution.....	8
6	Works Cited.....	9
7	PLAN CONCURRENCE .....	9
	ATTACHMENT 1: PERFORMANCE REQUIREMENTS SUMMARY .....	10
	ATTACHMENT 2: GOVERNMENT QA REPORT FORMAT .....	12
	ATTACHMENT 3: CONTRACTOR QUALITY CONTROL REPORT FORMAT.....	13
	ATTACHMENT 4: CONTRACTOR PRODUCTION REPORT FORMAT .....	14
	ATTACHMENT 5: ACCEPTANCE TEST SAMPLING PLAN .....	15
	ATTACHMENT 6: ROLES AND RESPONSIBILITIES MATRIX.....	16

# QUALITY ASSURANCE SURVEILLANCE PLAN

## 1 INTRODUCTION

This quality assurance surveillance plan (QASP) is pursuant to the requirements listed in the Task Order and modifications (TO) performance work statement (PWS). This QASP sets forth the procedures, guidelines, roles, and responsibilities. QASP implementation will be led by Naval Facilities Engineering and Expeditionary Warfare Center (EXWC) with support from NAVFAC Hawaii. The Government Technical team (GTT) will use this QASP to ensure the required performance standards are achieved by the contractor. The GTT consists of the PM, COR, CSE, CSET, and any technical specialist performing QA duties upon the request or on behalf of the KO or a GTT member.

### 1.1 Purpose

1.1.1 The purpose of the QASP is:

- (a) Describe methods used to monitor performance
- (b) Provide guidelines for systematic inspection and documentation of contractor activities
- (c) Provide reasonable assurance that the completed work will meet or exceed the requirements of the contract
- (d) Identify required documentation
- (e) List roles and responsibilities for the resources to be employed.

This QASP provides guidance for evaluating whether or not the contractor is meeting the performance standards and quality levels identified in the TO requirements and the contractor's quality control plan (QCP). The primary objective of the warranty work addressed by this QASP is the reinspection, repair, and return to service of Red Hill Fuel Storage Tank 5. A secondary objective is to determine the existence and location of free product, if any, and to recover free product to the extent possible.

Aspects of the project require an enhanced level of effort which is above and beyond ordinary NAVFAC QA surveillance activity.

1.1.2 The Quality Assurance (QA) work identified in this QASP has aspects which require an increased level of effort (LOE). EXWC is responsible for the management of the project technical team for inspection, testing, and repair of fuel system facilities. The Project Manager (PM) role is defined in Section 2.3 of this QASP. ACO authority is at EXWC ACQ72. The COR has been appointed at NAVFAC Hawaii. The CSE and CSET are contract employees of NAVFAC Hawaii and act under authority from the COR. The warranty work will be subject to high visibility and will be performed as part of an ongoing warranty repair action by the Contractor.

1.1.3 This QASP defines the roles and responsibilities of members of the GTT, identifies the performance objectives, defines the methodologies used to monitor and evaluate the contractor's performance, describes QA documentation requirements, and describes the analysis of QA monitoring results.

### 1.2 Performance Management Approach

- 1.2.1 This QASP will define the performance management approach taken by the GTT to monitor and manage the contractor's warranty work performance to ensure the expected outcomes communicated in the PWS are achieved. Performance management rests on developing a capability to review and analyze information generated through QA performance assessment. The ability to make decisions based on the analysis of performance and QC data is the cornerstone of performance management; this QA analysis yields information that indicate whether or not expected outcomes for the warranty work are being achieved by the contractor.
- 1.2.2 The performance-based approach identified in this QASP enables the contractor to play a large role in how the warranty work is performed. The proposed QA processes are designed to monitor contractor's performance within the stated constraints and if necessary, to stop contractor's work progress if deemed unacceptable. The exceptions to QA process reviews are prescriptive reviews as required by applicable federal, state, and local laws, along with compelling business situations such as unacceptable environmental, safety and health risks. The "results" focus of this QASP provides the contractor with flexibility to continuously improve and innovate over the course of the warranty work, but all work performed by contractor must maintain the critical outcomes expected.
- 1.2.3 As an enhancement to the performance-based approach, the GTT will execute proactive measures to validate contractor QC program output quality and data. These enhanced measures execute an acceptance sampling plan of attributes (NDE results) at a statistically significant level. The acceptance sampling plan is a valid method by which the quality of the QC program output can be determined by inspecting a representative sample of the entire population (Juran, 1988). Additional technical specialist resources may be utilized by the GTT to execute the plan. Should the acceptance sampling results be found less than the Acceptable Quality Level, corrective action steps will be taken as described in Section 5.

### **1.3 Performance Management Strategy**

- 1.3.1 The contractor is responsible for the workmanship and quality of all work performed. The contractor measures quality through the contractor's QC program. Contractor QC is work output. Therefore, QC includes all work performed, under this contract regardless of whether the work is performed by prime contractor's employees or by subcontractors. The contractor's QCP will set forth the staffing and procedures for self-inspecting the workmanship quality, timeliness, responsiveness, customer satisfaction, and other performance requirements in the PWS and warranty action. The contractor will develop and implement a performance management system with processes to assess its performance and contractor's PM will report its performance to the EXWC PM.
- 1.3.2 The NAVFAC Hawaii Facilities Engineering and Acquisitions Division (FEAD) Construction Surveillance Engineer (CSE) will monitor onsite performance and the EXWC PM will review performance reports furnished by the contractor to determine how the contractor is performing against communicated performance objectives. The EXWC PM will be the primary point of contact (POC) responsible for communicating corrective actions required to achieve critical outcomes and performance objectives. The contractor will be responsible for implementing corrective actions in QC processes and workmanship practices. The FEAD CSE will be the primary point of contact (POC) responsible for communicating the results of onsite QA assessments which verify contractor's QC personnel are effectively monitoring and documenting workmanship. Technical specialists such as third party QA technician(s) or government subject matter experts requested by the GTT will report to the contracting officer's representative (COR) or the onsite GTT member respectively.



## **2 ROLES AND RESPONSIBILITIES**

### **2.1 The Contracting Officer**

The EXWC Contracting Officer (KO), with support from the EXWC PM and the FEAD COR, is responsible for monitoring contract and warranty work compliance, including contract administration and cost control. The KO will resolve any differences between the observations documented by the GTT and the contractor. The KO has designated one FEAD COR as the government local authority for performance management of PWS and warranty action efforts. The FEAD COR has designated one FEAD CSE and one FEAD Construction Surveillance Engineering Technician (CSET) to support an increased LOE for field QA efforts.

### **2.2 The Contracting Officer's Representative**

The FEAD COR has been designated in writing by the EXWC KO to act as his or her authorized representative to assist in administering the TO and warranty action. COR limitations are contained in the written appointment letter. The COR is responsible for technical administration of the project and ensures proper government surveillance of the contractor's performance. The COR is not empowered to make any contractual commitments or to authorize any contractual changes on behalf of the Government. Any changes that the contractor deems may affect TO price, terms, or conditions will be referred to the KO for action. The COR will have the responsibility for collecting and/or completing QA Reports used to document the inspection and evaluation of the contractor's workmanship and QC performance. CSE and CSET surveillance will occur under the inspection of services clause for the warranty action relating to the TO.

### **2.3 The Project Manager**

The EXWC PM is responsible to EXWC for technical oversight of the fuel system inspection, testing, and repair as required to meet PWS objectives. The PM may engage technical specialists as-required to ensure objectives of this QASP are met. The PM is not empowered to make any contractual commitments or to authorize any contractual changes on behalf of the Government. Any changes that the contractor deems may affect contract price, terms, or conditions shall be referred to the KO for action. The PM, with field support from the CSE, will have the primary responsibility for (a) reviewing QA reports, (b) assessing Contractor inspection performance and results via periodic onsite surveillance, (c) assessing Contractor testing performance and results via periodic onsite surveillance, (d) and evaluating Contractor QC reports, as the basis for determining whether or not project objectives are being met. The PM is authorized to stop work in the event of a severe hazard exposure pursuant to 01 35 26.05 20. PM surveillance may occur under the inspection of services clause for any service relating to the TO. The PM will serve as the COR for a third party QA specialist utilized.

### **2.4 Construction Surveillance Engineer**

The CSE supports the COR, PM, and KO. CSE limitations are managed by the FEAD. The CSE is responsible for (a) the field administration of safety and environmental compliance, (b) contractor's site access, (c) coordination with the NAVFAC customer's POC, and (d) field surveillance of TO and warranty work. The CSE will support the KO or PM upon request to obtain and provide more information on a particular QA matter. The CSE is not empowered to make any contractual commitments, authorize any contractual changes on behalf of the Government, or direct technical performance with regard to the warranty inspection, QC testing, or rework of repairs. Any changes that the CSE or the contractor deems may affect contract price, terms, or conditions will be referred to the KO for action. Within the noted area of responsibility, the CSE will be responsible for preparing QA Reports used to document the inspection and evaluation of contractor workmanship and QC performance. The CSE and CSET are authorized to stop work in the event of a severe safety, security, or environmental

hazard exposure. CSE surveillance will occur under the inspection of services clause for the warranty action relating to the TO.

## **2.5 Construction Surveillance Engineering Technician**

The CSET will perform routine regular onsite surveillance of contractor activities on behalf of the KO. The CSET is responsible for observing and reporting contractor's progress in accomplishing the warranty inspection, QC testing, and rework of repairs. The CSET will assist the CSE in ensuring workmanship and QC performance objectives of the TO and warranty action are being met. The CSET will (a) review contractor's reports, testing personnel credentials, and equipment calibration certificates, and (b) attend contractor's field QC meetings. The CSET will provide exceptions or comment to the contractor's QC report in the QA Report portion as depicted in Attachment 4. The CSET will provide all findings to the CSE in daily QA reports, the format of which is in Attachment 2. The CSE is not empowered to make any contractual commitments or authorize any contractual changes on behalf of the Government. The CSET is authorized to stop work in the event of a severe safety, security, or environmental hazard exposure. Any changes that the CSET or contractor deems may affect contract price, terms, or conditions will be referred to the KO for action. QA surveillance by the CSET will occur under the inspection of services clause for the warranty action relating to the TO.

## **2.6 Quality Assurance Inspector**

The Quality Assurance Inspector (QAI) is a third party A/E who will perform onsite surveillance of contractor activities and report to the GTT. The specific scope of the QAI activity and level of effort is described in a separate contract action task order statement of work. The QAI is responsible for observing and reporting contractor's progress in accomplishing the warranty inspection, QC testing, and rework of repairs. The QAI will assist the GTT in observing the workmanship and QC performance objectives of the TO and warranty action are being met. The QAI will review contractor's reports, testing personnel credentials, and equipment calibration certificates, review the API inspection, and witness leak testing and other ND examinations. The QAI will provide all findings in reports. The QAI is not empowered to direct contractor activity, make any contractual commitments, or authorize any contractual changes.

## **3 METHODOLOGIES TO MONITOR PERFORMANCE**

Measures undertaken to provide an increased, overlapping, and redundant LOE of QA performance management include the following:

- a) Daily frequency of routine and regular field surveillance activities will be used by the FEAD to evaluate contractor's workmanship and QC performance.
- b) GTT access to regularly updated contractor QC Log.
- c) Redundant scrutiny of QA and QC documentation.
- d) Periodic field surveillance of inspection and testing results.
- e) Non-periodic, comprehensive field surveillance of accomplished work.
- f) Validation of the contractor QC Program results by execution of an acceptance sampling plan.

The warranty work to be performed is primarily rework which is critical to the viability of the customer's mission-essential Red Hill Fuel Storage Facility. The GTT will strive to assess QA requirements objectively but will verify acceptable contractor performance is actually being achieved. Pursuant to BMS 1.5.5.1.4 "Ongoing Quality Assurance Actions", specific QA surveillance activities will be conducted based on contractor's weekly QC meetings and the three-week look-ahead schedule. The primary methods of QA surveillance are both proactive and participatory.

### **3.1 Proactive Surveillance Techniques**

The GTT will take an active role in verifying contractor inspection, testing, and repair results. The GTT will also validate the contractor QC Program results (QCP). Validation will take the form of randomly selecting completed repairs as-reported on the QC Log, and systematically verifying the result. Verification will take the form of requiring the contractor to repeat in the presence of the GTT, leak test and MT inspection which have been reported as “Passed” in the QC Log. Verification will take place by the GTT members in person from the suspended work platform. Validation will implement the acceptance sampling plan in Attachment 5.

- 3.1.1 Acceptance Sampling Plan – A method to provide evidence the QCP has met the performance goals required to return Tank 5 to service is to perform sampling inspection of completed repairs and make a decision prior to acceptance (Johnson, 1994) of the warranty work. The plan uses a single stage model with binomial probability distribution calculated no more than 5% chance of a Type II error (accepting an undetected defect). The model identifies the minimum number of random repairs (76) which will be acceptance tested at an AQL of 3. A failed test shall result in rework of the repair. If the number of test failures is below the AQL, the QC program output is validated. If the number of test failures is at or over the AQL, the QC program is rejected. Rejection of the QC program will trigger performance requirement corrective measures noted in Section 5.1 and Attachment 1. The acceptance sampling plan is in Attachment 5.
- 3.1.2 Periodic Onsite Verification – The PM will conduct periodic onsite verification of contractor’s means, methods, and results of inspection and testing. Leak testing, MT inspections, and review of weldments (API\_Standard\_1104, 2014) from the inspection basket will take place. The results of the verification will be documented in QA reports per Attachment 2. To obtain accurate results, the planned locations and time of planned onsite surveillance activities might not be communicated to Contractor in advance. Frequency of the periodic surveillance is planned to be minimum five days per month.
- 3.1.3 Periodic Onsite Verification – The CSE will conduct periodic onsite verification of contractor’s means, methods, and results of inspection and testing. Leak testing, MT inspections, and review of weldments (API\_Standard\_1104, 2014) from the inspection basket will take place. The results of the verification will be documented in QA reports per Attachment 2. To obtain accurate results, the planned locations and time of planned onsite surveillance activities might not be communicated to Contractor in advance. Frequency of the periodic surveillance is planned to be minimum two days per week.

### **3.2 Participatory Surveillance Techniques**

The GTT will participate in contractor QC program three phases of control system activities. The intent will be to shape the progress and effectiveness of the contractor’s quality control. Since the definable features of work are limited to a few, GTT participation will extend beyond Three Phase of Control meeting attendance. The primary daily GTT onsite member will be the CSET for minimum two hours.



- 3.2.1 Preparatory Phase – The GTT will participate in preparatory phase meetings prior to start of work of each definable feature of work. At the meeting the GTT will review the applicable specifications and references for the work. This will include welding specifications, NDE procedures, and testing protocol. The GTT will verify all materials and equipment have been brought onsite and have been tested and approved for use. An examination of the work area will take place to assure all required preliminary work has been completed. Review of the activity hazard analysis and discussion of the work procedures will also be performed.
- 3.2.2 Initial Phase – At the beginning of the work, the GTT will review preliminary QCP output, verify the adequacy of the QC controls, and assess workmanship. Corrective actions to address concerns shall be directed to the QCM and noted in the daily QA report.
- 3.2.3 Follow-Up Phase – The GTT will perform daily checks to assure continued compliance with contract requirements is taking place, including safety and control testing.
- 3.2.4 Daily Surveillance – The CSET will observe onsite contractor activity during various aspects of warranty work DFOW. This will include QA surveillance of contractor QC activities; review of contractor inspection activity to include operator credentials; review of contractor testing to include operator credentials; review of rework repair techniques, means, and methods; review of daily contractor reporting; preparation of a daily QA report. In an effort to obtain accurate results, the CSET observational activity will occur at intervals unknown to contractor and will not be readily predictable.
- 3.2.5 Daily Offsite Review – The PM will review Contractor daily QC and production reports, QC log, daily QA reports as necessary to monitor and assess contractor’s workmanship and QC performance. The PM reviews will form the basis for an ongoing determination of performance with regard to workmanship and QC performance objectives. The determination shall be provided periodically to the GTT, KO, and EXWC management for use in reply to stakeholder inquiry.
- 3.2.6 Daily Offsite Review – The CSE will review Contractor daily QC and production reports, QC log, daily CSET reports as necessary to monitor and assess contractor’s workmanship and QC performance. The CSE weekly assessments will form the basis for an ongoing determination of performance with regard to workmanship and QC performance objectives. The determination shall be provided periodically to the GTT, KO, and FEAD management for use in reply to stakeholder inquiry.
- 3.2.7 Non-Periodic Onsite Surveillance – The CSE will conduct non-periodic onsite surveillance of Contractor’s accomplished work for each DFOW milestone to ensure successful completion of all inclusive work tasks and related activities. In an effort to ensure comprehensive results, specifics of planned onsite surveillance activities will be communicated to Contractor in advance.
- 3.2.8 Periodic QC Meetings – The CSE and CSET will attend contractor’s weekly QC meetings. The CSE, with support from the CSET, will assess contractor’s warranty work planning and onsite progress. Attention will be directed to the contractor’s personnel assignments and individual performance capabilities in order to assess contractor’s overall ability to accomplish proposed workmanship and QC results.

### **3.3 Customer Feedback**

The contractor is expected to establish and maintain professional communication between its employees and Navy personnel. The primary objective of this communication is the Navy's customer satisfaction. Customer satisfaction is the most significant external indicator of the success and effectiveness of all services provided and can be measured through Navy and external stakeholders' complaints.

Performance management requires the contractor to be customer focused through initially and internally addressing customer complaints with the CSE and investigating the issues. The Navy and external stakeholders' retain the option to communicate complaints to the Navy POCs, as opposed to the contractor.

The COR will accept those customer complaints deemed valid after reviewing with contractor. The COR will investigate valid complaints to the extent necessary to resolve effectively and timely.

Customer feedback will be obtained by the CSE and CSET during weekly meetings with Navy stakeholders. Customer feedback summaries will be provided to contractor by the CSE and CSET during contractor's weekly QC meetings.

### **3.4 Acceptable Quality Levels**

The acceptable quality levels (AQLs) are included in Attachment 1, "Performance Requirements Summary Table". The AQLs for contractor performance are structured to allow the contractor to manage how the work is performed, while providing negative incentives for performance shortfalls. For certain critical activities, e.g. those involving the submission and adherence to an Accident Prevention Plan (APP) as outlined in Specification 01 35 26.05 20 and 385-1-1, the desired performance level is established at 100 percent.

## **4 QUALITY ASSURANCE DOCUMENTATION**

### **4.1 The Performance Management Feedback Loop**

The performance management feedback loop begins with the communication of expected outcomes. Performance standards are expressed in the PWS and WP. Performance standards are assessed using the performance monitoring techniques provided in Attachment 1.

### **4.2 Quality Assurance Reports**

The QA surveillance will be accomplished by the GTT and will be reported using the QA Report provided in Attachment 2 and the QA Report portion of the Contractor Quality Control Report provided in Attachment 3. The completed QA reports will document the GTT's assessment of the contractor's performance under the TO and warranty action to ensure the required workmanship and QC results are being achieved.

4.2.1 The COR and PM will retain a copy of all completed QA Reports from the CSE and CSET.

## **5 ANALYSIS OF QUALITY ASSURANCE ASSESSMENT**

### **5.1 Determining Performance**

5.1.1 The GTT will use the monitoring methods cited to determine whether the performance standards, service levels and AQLs have been met. If the contractor has not fully met the requirements, the contractor will be required to develop a corrective action plan to show how and when contractor's performance will be restored to the required levels.

- 5.1.2 Should the AQL prescribed in Acceptance Test Sampling Plan (Attachment 5) not be met, notification shall be provided to the contractor in the form of a notice of non-compliance. Should no extenuating circumstances be found by the Contracting Officer, the contractor QCM shall be determined to be incompetent, careless, or otherwise objectionable per FAR 52.236-5. The result of that determination shall be ineligibility from working on the project. The KO shall determine whether additional contractual steps as detailed in Attachment 1 are warranted.

## **5.2 Reporting**

- 5.2.1 eProjects: Twice per month the PM will update the associated eProjects status notes summarizing contractor's progress. Once per month, the PM will update the eProjects status notes summarizing the overall results of the QA surveillance efforts. The summary will consider the contractor's progress reports and the quality assurance reports. This will become part of the QA documentation. This documentation process will enable the GTT to demonstrate whether or not the contractor is meeting the stated QA objectives and performance standards, including cost, technical and scheduling objectives.
- 5.2.2 eContracts: Once per week the CSE will update the associated eContracts record summarizing contractor progress. Once per month, the CSE will update the eContracts record summarizing the overall status of contractor's fieldwork progress.
- 5.2.3 Stakeholder: Updates provided to stakeholders will be coordinated within the GTT for content prior to release. Release shall only be made in accordance with the REDHILL Communications Plan Process.

## **5.3 Reviews and Resolution**

- 5.3.1 The Contractor's PM, QC Manager and Project Engineer will meet in person or via teleconference with the PM, CSE and CSET on a weekly basis to discuss progress and performance. The GTT will conduct in-depth reviews with the contractor on a monthly basis, including self-assessments by the contractor. The CSE will meet with the contractor when required by the GTT or upon the Contractor's request. The agenda of the reviews will include:
- 5.3.1.1 Monthly performance assessment
  - 5.3.1.2 Issue resolution and concerns
  - 5.3.1.3 Three-week look-ahead review and project schedule progress review against the baseline, including corrective action plan review
  - 5.3.1.4 Recommendations for lessons-learned and corrective actions
- 5.3.2 The GTT must coordinate and communicate with the contractor's onsite key personnel in a timely manner to resolve instances or concerns regarding marginal or unacceptable performance.
- 5.3.3 The PM and contractor's key personnel will jointly formulate long-term courses of action based on progress. Decisions regarding changes to metrics, thresholds, or service levels should be clearly documented in correspondences or meeting minutes. Changes to service levels, procedures, and metrics which will result in a contract modification shall be avoided.



## 6 Works Cited

- API\_Standard\_1104. (2014). *Welding of Pipelines and Related Facilities*. Washington, DC: American Petroleum Institute.
- Grant, E. L., & Leavenworth, R. S. (1988). *Statistical Quality Control Fifth Edition*. New York: McGraw-Hill Book Company.
- Johnson, R. A. (1994). *Miller and Freund's Probability and Statistics for Engineers*. Englewood Cliffs: Prentice-Hall, Inc.
- Juran, J. M. (1988). *Juran's Quality Control Handbook Fourth Edition*. New York: McGraw-Hill Book Company.

## 7 PLAN CONCURRENCE

### **Acceptance Satisfactory To the Participants – Sat-To**

This QASP documents organizational coordination and quality assurance activities for the warranty phase repairs of Red Hill Tank 5, JBPHH. Component coordination is between NAVFAC Engineering and Expeditionary Warfare Center (EXWC), NAVFAC PAC, and NAVFAC Hawaii FEAD (NFHI). Concurrence is provided to ensure the QASP has been reviewed, meets organizational requirements, and is satisfactory to the participants.

#### Concurrence

EXWC PM  
EXWC CIBL  
NFHI COR  
NFHI CIBL

Concurrence provided on separate document.


**ATTACHMENT 1: PERFORMANCE REQUIREMENTS SUMMARY**

<b>Required Services (Tasks)</b>	<b>Performance Standards</b>	<b>Acceptable Quality Levels</b>	<b>Methods of Surveillance</b>	<b>Performance Corrective Measures</b>
Submittals in accordance with Task Order requirements	99% of submittals accurately depict current status	97%	File reviews, periodic inspections, random, observations,	Contractor Performance Assessment Reports System (CPARS) Review
Administer quality control program including subcontractor management in accordance with QCP	Contractor is in compliance with QCP 97% of the time	97%	File reports, periodic inspections, random, observations,	CPARS Review Notice of Non-Compliance Letter of Concern Cure Notice
Preparation of comprehensive list of weld inspection/NDE/repair locations for QC and QA tracking	All previous repair locations	100% of locations uniquely identified	Review/editing of draft versus existing documentation and actual conditions	Notice of Non-Compliance Letter of Concern
Documentation of NDE inspection results	Objective Pass-Fail	100% of locations on comprehensive list tested and passed	<ol style="list-style-type: none"> <li>Ongoing visual surveillance of onsite activity by QAT</li> <li>Review Daily QC Reports</li> <li>Un-announced validation of inspection NDE results on random locations by QAT or PM</li> </ol>	Notice of Non-Compliance Letter of Concern Cure Notice
Govt: Validation of QCP	Acceptance Sampling Plan	3	<ol style="list-style-type: none"> <li>In-basket review of leak test, MT inspection, weldments</li> <li>Determine Pass:Fail</li> <li>Compare results to AQL</li> </ol>	Remove QC Manager Notice of Non-Compliance Letter of Concern Cure Notice

Required Services (Tasks)	Performance Standards	Acceptable Quality Levels	Methods of Surveillance	Performance Corrective Measures
Material and Workmanship Submittals	Contractor in compliance with SOW	97%	Work Plan, Daily Reports, Draft Report and Final Report Review	CPARS Review
Material and Workmanship: Repair of locations with failed NDE and/or unacceptable weld quality	Work in compliance with SOW and submittals through QC program IAW 01 45 00 05.20	100%	<ol style="list-style-type: none"> <li>1. Ongoing visual surveillance of onsite activity by QAT</li> <li>2. Review Daily Reports</li> <li>3. Un-announced validation of repair NDE results on random locations by QAT or PM</li> </ol>	CPARS Review Notice of Non-Compliance Letter of Concern Cure Notice
Draft Completion Report	Contractor in compliance with SOW	95%	Report Review	CPARS Review
Final Completion Report	Comments implemented as noted by reviewer	99% of agreed upon comments	Report Review	CPARS Review




## ATTACHMENT 2: GOVERNMENT QA REPORT FORMAT

<b>GOVERNMENT QUALITY ASSURANCE (QA) REPORT</b>		DATE
(ATTACH ADDITIONAL SHEETS IF NECESSARY)		REPORT NO
CONTRACT NO	TITLE AND LOCATION	
<b>STATUS</b>	WORKING? <input checked="" type="radio"/> YES <input type="radio"/> NO IF NO, WHY NOT:	<input type="button" value="Add"/> <input type="button" value="Del"/>
WEATHER CONDITIONS:		<input type="button" value="Add"/> <input type="button" value="Del"/>
<b>CHECK POINTS</b>	SUPERINTENDENT ON SITE <input type="radio"/> YES <input checked="" type="radio"/> NO REMARKS:	<input type="button" value="Add"/> <input type="button" value="Del"/>
	QC MANAGER ON SITE <input checked="" type="radio"/> YES <input type="radio"/> NO REMARKS:	<input type="button" value="Add"/> <input type="button" value="Del"/>
	QC REPORTS CURRENT <input type="radio"/> YES <input checked="" type="radio"/> NO REMARKS:	<input type="button" value="Add"/> <input type="button" value="Del"/>
	AS-BUILTS CURRENT <input checked="" type="radio"/> YES <input type="radio"/> NO REMARKS:	<input type="button" value="Add"/> <input type="button" value="Del"/>
	SUBMITTALS APPROVED FOR ONGOING WORK <input checked="" type="radio"/> YES <input type="radio"/> NO REMARKS:	<input type="button" value="Add"/> <input type="button" value="Del"/>
	DEFICIENCY LIST REVIEWED <input type="radio"/> YES <input checked="" type="radio"/> NO REMARKS:	<input type="button" value="Add"/> <input type="button" value="Del"/>
WORK OBSERVED/DEFICIENCIES NOTED/SAFETY ISSUES DISCUSSED/QA TESTS AND RESULTS:		<input type="button" value="Add"/> <input type="button" value="Del"/>
Schedule Act/My No	DESCRIBE OBSERVATIONS	
MEETING/CONFERENCE NOTES (INCLUDING PARTICIPANTS):		<input type="button" value="Add"/> <input type="button" value="Del"/>
Schedule Act/My No	NOTES	
INSTRUCTIONS GIVEN OR RECEIVED/CONTROVERSIES PENDING:		<input type="button" value="Add"/> <input type="button" value="Del"/>
Schedule Act/My No	INSTRUCTIONS/CONTROVERSIES	
		
QA REPRESENTATIVE	DATE	SUPV INITIALS
		DATE

### ATTACHMENT 3: CONTRACTOR QUALITY CONTROL REPORT FORMAT

<b>CONTRACTOR QUALITY CONTROL REPORT</b> <small>(ATTACH ADDITIONAL SHEETS IF NECESSARY)</small>				DATE
				REPORT NO
PHASE	CONTRACT NO	CONTRACT TITLE		
<b>PREPARATORY</b>	WAS PREPARATORY PHASE WORK PERFORMED TODAY? IF YES, FILL OUT AND ATTACH SUPPLEMENTAL PREPARATORY PHASE CHECKLIST.			<input type="radio"/> YES <input type="radio"/> NO
	Schedule Activity No	Definable Feature of Work (DFOW)	Index#	
<b>INITIAL</b>	WAS INITIAL PHASE WORK PERFORMED TODAY? IF YES, FILL OUT AND ATTACH SUPPLEMENTAL INITIAL PHASE CHECKLIST.			<input type="radio"/> YES <input type="radio"/> NO
	Schedule Activity No	Definable Feature of Work (DFOW)	Index#	
<b>FOLLOW-UP</b>	WORK COMPLIES WITH CONTRACT AS APPROVED DURING INITIAL PHASE?			<input type="radio"/> YES <input type="radio"/> NO
	WORK COMPLIES WITH SAFETY REQUIREMENTS AND INSPECTION COMPLIES WITH EM385-1-17			<input type="radio"/> YES <input type="radio"/> NO
Schedule Activity No	Description of Work, Testing Performed & By Whom, Definable Feature of Work, Specification Section, Location and List of Personnel Present			
REWORK ITEMS IDENTIFIED TODAY (NOT CORRECTED BY CLOSE OF BUSINESS)		REWORK ITEMS CORRECTED TODAY (FROM REWORK ITEMS LIST)		
Schedule Activity No	Description	Schedule Activity No	Description	
REMARKS (Also Explain Any Follow-Up Phase checklist Item From Above That Was Answered "NO"; Work Deficiency, Safety Deficiency.) Manuf. Rep On-Site, etc.				Add Del
Schedule Activity No	Description			
<p style="font-size: small;">On behalf of the contractor, I certify that this report is complete and correct and equipment and material used and work performed during this reporting period is in compliance with the contract drawings and specifications to the best of my knowledge except as noted in this report.</p> <div style="display: flex; justify-content: space-between; align-items: flex-end; margin-top: 10px;"> <div style="border-bottom: 1px solid black; width: 60%;"></div> <div style="font-size: x-small; text-align: center;">AUTHORIZED QC MANAGER AT SITE</div> <div style="border-bottom: 1px solid black; width: 20%;"></div> <div style="font-size: x-small; text-align: center;">DATE</div> </div>				
<b>GOVERNMENT QUALITY ASSURANCE REPORT</b>				DATE
QUALITY ASSURANCE REPRESENTATIVE'S REMARKS AND/OR EXCEPTIONS TO THE REPORT: FOR GOVERNMENT USE ONLY.				Add Del
Schedule Activity No	Description			
<div style="display: flex; justify-content: space-between; align-items: flex-end; margin-top: 10px;"> <div style="border-bottom: 1px solid black; width: 60%;"></div> <div style="font-size: x-small; text-align: center;">GOVERNMENT QUALITY ASSURANCE MANAGER</div> <div style="border-bottom: 1px solid black; width: 20%;"></div> <div style="font-size: x-small; text-align: center;">DATE</div> </div>				

# ATTACHMENT 4: CONTRACTOR PRODUCTION REPORT FORMAT

<b>CONTRACTOR PRODUCTION REPORT</b> <small>(ATTACH ADDITIONAL SHEETS IF NECESSARY)</small>					DATE _____	
CONTRACT NO _____		TITLE AND LOCATION _____			REPORT NO _____	
CONTRACTOR _____				SUPERINTENDENT _____		
AM WEATHER _____		PM WEATHER _____		MAX TEMP (F) _____	MIN TEMP (F) _____	
WORK PERFORMED TODAY						
Add	Del					
Schedule Activity No	WORK LOCATION AND DESCRIPTION	EMPLOYER	NUMBER	TRADE	HRS	
<b>JOB SAFETY</b>		WAS A JOB SAFETY MEETING HELD THIS DATE? (If YES attach copy of the meeting minutes)		<input type="radio"/> YES <input type="radio"/> NO	TOTAL WORK HOURS ON JOB SITE THIS DATE, INCL CONT SHEETS	
		WERE THERE ANY LOST TIME ACCIDENTS THIS DATE? (If YES attach copy of completed OSHA report)		<input type="radio"/> YES <input type="radio"/> NO	CUMULATIVE TOTAL OF WORK HOURS FROM PREVIOUS REPORT	
		WAS CRANE/MANLIFT/TRENCHING/SCAFFOLD/HV/ELEC/HIGH WORK/HAZMAT WORK DONE? (If YES attach statement or checklist showing inspection performed)		<input type="radio"/> YES <input type="radio"/> NO	TOTAL WORK HOURS FROM START OF CONSTRUCTION	
		WAS HAZARDOUS MATERIAL/WASTE RELEASED INTO THE ENVIRONMENT? (If YES attach description of incident and proposed actions.)		<input type="radio"/> YES <input type="radio"/> NO		
Schedule Activity No	LIST SAFETY ACTIONS TAKEN TODAY/SAFETY INSPECTIONS CONDUCTED			<input type="checkbox"/> SAFETY REQUIREMENTS HAVE BEEN MET		Add    Del
EQUIPMENT/MATERIAL RECEIVED TODAY TO BE INCORPORATED IN JOB (INDICATE SCHEDULE ACTIVITY NUMBER)						
Add	Del					
Schedule Activity No	Submittal #	Description of Equipment/Material Received				
CONSTRUCTION AND PLANT EQUIPMENT ON JOB SITE TODAY. INDICATE HOURS USED AND SCHEDULE ACTIVITY NUMBER.						
Add	Del					
Schedule Activity No	Owner	Description of Construction Equipment Used Today (Incl Make and Model)				Hours Used
Add	Del					
Schedule Activity No	REMARKS					
 _____ CONTRACTOR/SUPERINTENDENT			_____ DATE			



## ATTACHMENT 5: ACCEPTANCE TEST SAMPLING PLAN

### Acceptance Test Sampling Plan

Acceptance sampling is a valid method by which the quality of the QC program output can be obtained by inspecting a representative sample of the entire population. By examining a series of samples, information is obtained about the entire process (Juran, 1988).

Since information about the process, in this case the QC program output, is of interest, Type B sampling of attributes plan was selected. In the plan samples are chosen at random from all repairs reported as complete by the QC program. Witness testing will be performed to classify the repair as conforming or non-conforming. The number of non-conforming repairs will be compared to an acceptance number,  $c$ , identified in the plan and a decision made to accept or reject the entire lot (QC program output) if the acceptance number is exceeded.

The plan uses a single-stage model which will specify the quality level, lot tolerance percent defective (LTPD) of the QC program output at the specified risk of accepting an undetected defect,  $\beta$ . The model was optimized to reduce the sample size while maintaining no more than 5% risk of a Type II ( $\beta$ ) error. The binomial was used as a good approximation of the probability distribution for an attributes sampling plan (Grant, 1988). The sampling plan and results are below.

	Variable	Definition	Value
Input	N	Population size	677
	LTPD	Lowest quality, or the highest proportion of defective results to total number of repairs, still acceptable	10%
	AQL	Acceptable quality level: Ideal percentage of defects	2%
Output	n	Sample size	76
	c	Maximum number of failures before entire QC program output is rejected	3
	$\beta$	Chance of accepting an undetected defect	4.7%

By acceptance sampling 76 repair locations reported to have passed QC program output, the GTT will have no more than a 5% chance of unknowingly accepting an undetected defect should no more than three defects be discovered. Should more than three defects be discovered, the entire QC program output is rejected.

**ATTACHMENT 6: ROLES AND RESPONSIBILITIES MATRIX**

	Phase		Element	QCM (Ktr)	FEAD	EXWC
<b>Inspection</b>	<b>Leak Testing</b>	Submittal Process	<b>Procedure</b> - Verify contractor provided complete NDE LTE-1 testing procedure including operator certifications as-required	A	QA	QA
		Field Visit	<b>Testing</b> - Perform leak testing on repairs per NDE-LT-1.	A	QA	QA
		Field Visit	<b>Quality Control Program Output</b> - Report specific leak testing status of each repair site in QC Log.	A	QA	QA
			<b>Acceptance Testing</b> - Verify QC Program output with random acceptance sampling. Verify leak testing procedure meets NDE-LT-1 and API 653 Section 12. Witness leak testing from the inspection basket.	—	V	V
	<b>Weldments</b>	Field Visit	<b>Visual inspection</b> - Verify weldments meet criteria of API 653 Section 12, API 1104.	A	QA	QA
			<b>Testing</b> - Perform MT on weldments per MT-3.	A	QA	QA
			<b>Inspection</b> - Perform liquid penetrant inspection per PT-1 on weldments.	A	QA	QA
			<b>Quality Control Program Output</b> - Report visual inspection, PT inspection, and MT testing results of each repair site in QC Log.	A	QA	QA
			<b>Acceptance Testing</b> - Verify QC Program output with random acceptance sampling. Witness MT inspections (MT-3 Yoke Technique, Wet Fluorescent Magnetic Particle Method), PT (PT-1 Liquid Penetrant Inspection by Visible Dye Method) and review of weldments (API Standard 1104) from the inspection basket.	—	V	V
	<b>Hold Point</b>					

	Phase	Element	QCM(Ktr)	FEAD	EXWC	
<b>Repair</b>	<b>Welding</b>	Submittal Process	<b>Welding Plan</b> - Provide appropriate WPS and PQR	A	QA	QA
		Submittal Process	<b>Welder Credentials</b> - Provide welder certifications. Verify meet requirements of API 653 Section 11 and WPS	A	QA	QA
		Field Visit	<b>Inspection</b> - Visual verification weldments meet criteria of API 653 Section 12, API 1104.	A	QA	QA
		Field Visit	<b>Testing</b> - Perform leak testing on repairs per NDE-LT-1.	A	QA	QA
		Field Visit	<b>Testing</b> - Perform MT on repairs per MT-3.	A	QA	QA
		Field Visit	<b>Inspection</b> - Perform liquid penetrant inspection per PT-1 on repairs.	A	QA	QA
		Field Visit	<b>Quality Control Program Output</b> - Report specific visual inspection and MT results of each repair site in QC Log.	A	QA	QA
		Field Visit	<b>Testing</b> - Verify QC Program output with random acceptance sampling. Witness MT inspections (MT-3 Yoke Technique, Wet Fluorescent Magnetic Particle Method), PT (PT-1 Liquid Penetrant Inspection by Visible Dye Method) and review of weldments (API Standard 1104) from the inspection basket.	—	V	V
	<b>Coating</b>	Submittal Process	<b>Coating</b> - Provide material submittals in accordance with 09 97 13.15 LOW VOC POLYSULFIDE INTERIOR COATING OF WELDED STEEL PETROLEUM FUEL TANKS	A	S	S
		Submittal Process	QP-5 Inspector qualifications	A	S	S
		Field Visit	<b>Inspection</b> - Verify surface preparation in accordance with 09 97 13.15 Part 3.	A	QA	QA
		Field Visit	<b>Testing</b> - Perform holiday testing	A	QA	QA
		Field Visit	<b>Testing</b> - Verify coating thickness	A	QA	QA
		Field Visit	<b>Quality Control Program Output</b> - Report specific visual inspection and MT results of each repair site in QC Log.	A	QA	QA

KEY = A - Approve, R - Review, W - Witness, RA - Receipt Acknowledge, S - Surveillance Review, V- Verification and Testing, C - Copy, QA - Quality Assurance



**DEFINITIONS**

Approve	(A)	Professional or quality control endorsement of the submittal or installed system meets the contract requirements
Review	(R)	To confirm accuracy of the submittal and that it meets contract requirements
Witness	(W)	Observe demonstration of system performance for acceptance
Receipt Acknowledge	(RA)	Confirm receipt of submittal with no review necessary
Surveillance Review	(S)	A quality assurance review based on risk, complexity, and workload
Performance Verification and Acceptance Testing	(V)	A demonstration of satisfactory construction and system performance
Receive Copy of Correspondence	(C)	Receive a copy of the transmittal sheet and/or correspondence letter
Quality Assurance Inspection	(QA)	Witnessing satisfactory performance without testing all devices or visual inspection of various parts of the system

**END QUALITY ASSURANCE SURVEILLANCE PLAN**



**Section 2.0 – Suitability for Service Statement**

**Suitability for Service Statement  
Tank 5 – Certificate of Compliance  
UST Tank 5 Redhill Complex – Pearl Harbor, HI**

Tank 5 integral structural and component integrity is suitable for continued service at the specified operation interval and can be placed back in normal operation.

The Tank 5 repairs identified for mandatory repairs for continued service, along with the short term ≤ 10 yr. and long term ≤ 20 yr. repairs for the desired operational interval have been successfully completed. After the repairs were completed, the repairs were re-inspected and tested. All repairs were found acceptable and approved for return to normal operation for continued service.

The next API-653 internal inspection should be conducted in twenty (20) years, or by May 2033. The bottom life calculations determined the tank bottom to have greater than twenty (20) years of remaining operation. A visual inspection of UST internal coatings should be conducted in in twenty (20) years with the internal inspection. A visual inspection of UST external surfaces should be conducted monthly by operations personnel to observe for signs of tank or component damage, accelerated deterioration or abnormalities. Any relevant observations should be promptly evaluated to determine any change in suitability.

Note: This certificate of compliance and suitability for service is based on continued normal operation in the same service conditions for Tank 5. Any intended change in service, product, operations or conditions to the tank should be re-evaluated prior to making the change to determine if it is a relevant change and if the tank will continue to be suitable for the desired service, product, operations or conditions. Any changes in service, product, operations or conditions will void this certificate of compliance and suitability for service.

API-653 Inspector:

SIGNATURE ON FILE – HAND SIGNED COPY WILL BE IN FINAL REPORT COPIES

Tim D. Anderson; API-510 Pressure Vessels / API-570 Piping / API-653 Aboveground Tanks # 494/37258  
AWS-CWI / ASNT NDT LvL III MT, PT, UT, VT & RT

Professional Engineer’s Review:

**Tim**

SIGNATURE ON FILE – HAND SIGNED COPY WILL BE IN FINAL REPORT COPIES

Digitally signed by Tim Anderson  
DN: cn=Tim Anderson,

email=timothy.anderson@willbros.com, c=US

Thomas Fulton, P.E. – Oklahoma / California P.E. Registration Number

**Anderson**

Date: 2013.06.27 13:05:32 -05'00'