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MEMORANDUM

THEORETICAL PERFORMANCE OF LIQUID HYDROGEN WITH
LIQUID OXYGEN AS A ROCKET PROPELLANT

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NATIONAL AERONAUTICS AND
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Tables II(a) through II(h): Add 10,000 to the enthalpy values for $R = 0.150$ and 0.200 for pressure ratios of 1.00 to 4000.00.

Tables II(a), (c), (d), (e), (g), and (h): Add 10,000 to the enthalpy values for $R = 0.250$ for pressure ratios of 1.00 to 10.00.

Tables II(b) and (f): Add 10,000 to the enthalpy values for $R = 0.250$ for pressure ratios of 1.00 to 10.21.

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SUMMARY

Theoretical rocket performance for both equilibrium and frozen composition during expansion was calculated for the propellant combination liquid hydrogen and liquid oxygen at four chamber pressures (60, 150, 300, and 600 lb/sq in. abs) and a wide range of pressure ratios (1 to 4000) and oxidant-fuel ratios (1.190 to 39.683). Data are given to estimate performance parameters at chamber pressures other than those for which data are tabulated. The parameters included are specific impulse, specific impulse in vacuum, combustion-chamber temperature, nozzle-exit temperature, molecular weight, molecular-weight derivatives, characteristic velocity, coefficient of thrust, ratio of nozzle-exit area to throat area, specific heat at constant pressure, isentropic exponent, viscosity, thermal conductivity, Mach number, and equilibrium gas compositions.

The maximum value of specific impulse for expansion to 1 atmosphere is given in the following table:

Combustion-chamber pressure, P_c , lb/sq in. abs	Ratio of chamber pressure to exit pressure, P_c/P	Specific impulse, I, (lb)(sec)/(lb)	
		Assuming frozen composition	Assuming equilibrium composition
60	4.083	254.6	255.4
150	10.207	313.1	315.0
300	20.414	345.8	348.1
600	40.827	371.8	374.5

INTRODUCTION

The performance of hydrogen and oxygen as a rocket propellant has been reported in the literature. However, additional performance calculations are needed for a wider range of conditions than were heretofore available. Calculations were therefore made at the NASA Lewis Research Center to provide rocket performance data for liquid hydrogen and liquid oxygen for the following conditions:

- (1) Four chamber pressures (60, 150, 300, and 600 lb/sq in. abs)
- (2) A wide range of oxidant-fuel weight ratios (1.190 to 39.683)
- (3) A wide range of pressure ratios (1 to 4000)
- (4) Equilibrium and frozen composition during expansion

Data are given to permit estimates of performance parameters at chamber pressures other than those given in this report.

SYMBOLS

The following symbols are used in this report:

A	nozzle area, sq in.
\mathfrak{A}	number of formula weights (defined as A in ref. 1)
a	local velocity of sound, ft/sec
C_F	coefficient of thrust, $C_F = g_c I/c^*$ = $F/P_c A_t$
C_p^o	molar specific heat at constant pressure, cal/(mole)(°K)
c_p	specific heat at constant pressure, $(\partial h/\partial T)_P$, cal/(g)(°K)
c_v	specific heat at constant volume, cal/(g)(°K)
c^*	characteristic velocity, $g_c P_c A_t / w$, ft/sec
F	thrust, lb
$f_\mu^{(k)}$	function of T^*
g_c	gravitational conversion factor, 32.174 $\left(\frac{\text{lb mass}}{\text{lb force}}\right) \left(\frac{\text{ft}}{\text{sec}^2}\right)$

H_T^0	sum of sensible enthalpy and chemical energy at temperature T , cal/mole
h	sum of sensible enthalpy and chemical energy per unit mass, $\frac{\sum_i x_i (H_T^0)_i}{\mu}, \text{ cal/g}$
I	specific impulse with ambient and exit pressures equal, (lb force)(sec)/lb mass
I_{vac}	specific impulse in vacuum, (lb force)(sec)/lb mass
k	coefficient of thermal conductivity, cal/(sec)(cm)(°K)
M	Mach number
μ	molecular weight, $\sum_i x_i \mu_i$, g/g-mole or lb/lb-mole
n_c^*	characteristic-velocity exponent, $\partial \ln c^* / \partial \ln P_c$
n_I	specific-impulse exponent for fixed pressure ratio, $\left(\frac{\partial \ln I}{\partial \ln P_c} \right)_{P_c/P}$
$n_{I_{vac}}$	specific-impulse in vacuum exponent for fixed pressure ratio, $\left(\frac{\partial \ln I_{vac}}{\partial \ln P_c} \right)_{P_c/P}$
n_T	temperature exponent for fixed pressure ratio, $\left(\frac{\partial \ln T}{\partial \ln P_c} \right)_{P_c/P}$
n_ϵ	area-ratio exponent for fixed pressure ratio, $\left(\frac{\partial \ln \epsilon}{\partial \ln P_c} \right)_{P_c/P}$
O/F	oxidant-fuel weight ratio
P	static pressure (sum of partial pressures), lb/sq in. abs
p	partial pressure, lb/sq in. abs
Q	heat of formation or dissociation

R	equivalence ratio, ratio of two times the number of oxygen atoms to the number of hydrogen atoms, $2(O)/(H)$
\mathcal{R}	universal gas constant (consistent units)
S_T^0	entropy at a pressure of 1 atmosphere, cal/(mole)(°K)
s	entropy per unit mass, $\frac{\sum_i x_i [(S_T^0)_i - \mathcal{R} \ln(p_i/14.696)]}{M}$, cal/(g)(°K)
T	temperature °K
T^*	reduced temperature for viscosity calculations (temperature divided by force constant (ϵ/k)), kT/ϵ
v	velocity, ft/sec
v	specific volume
w	mass-flow rate, lb/sec
x	mole fraction
γ	isentropic exponent, $(\frac{\partial \ln P}{\partial \ln \rho})_s$
δ	correction term for polarity for viscosity calculations
ϵ	ratio of nozzle area to throat area
ϵ/k	force constant for viscosity calculation
μ	absolute viscosity, g/(cm)(sec) or poises
ρ	density, lb/cu in.
σ	collision diameter for viscosity calculation
$\Omega(2,2)^*$	function of T^*

Subscripts:

c	combustion chamber
e	nozzle exit

i product of combustion
 in injector
 P constant pressure
 P_c/P constant pressure ratio
 s constant entropy
 T constant temperature
 t nozzle throat
 l reference point

Superscript:

\circ thermodynamic standard reference state

CALCULATION OF PERFORMANCE DATA

Theoretical rocket performance data were obtained for liquid hydrogen with liquid oxygen for four chamber pressures over a wide range of oxidant-fuel ratios and pressure ratios assuming both equilibrium and frozen composition during expansion.

The computations were carried out by the method of reference 1 with modifications to adapt it for use with an IBM 650 Magnetic Drum Data-Processing Machine, with index accumulators, high-speed core, and floating-point attachments. The successive approximation process used in the calculations was continued until seven-figure accuracy was reached in the desired values of the assigned parameters (mass balance, pressure, and enthalpy or entropy).

Assumptions

The calculations were based on the following usual assumptions: perfect gas law, adiabatic combustion at constant pressure, isentropic expansion, no friction, homogeneous mixing, and one-dimensional flow. The products of combustion were assumed to be the following ideal gases: atomic hydrogen, H; hydrogen, H₂; water, H₂O; atomic oxygen, O; oxygen, O₂; and the hydroxyl radical, OH.

Initial Data

Thermodynamic data. - The ideal gas thermodynamic properties for atomic hydrogen, hydrogen, atomic oxygen, and oxygen were taken from reference 2. Data for water are also given in reference 2, however, the same data are given to more decimal places in reference 3, and therefore reference 3 data were used. The hydroxyl radical data were taken from reference 4. The values of entropy used in the present report do not include nuclear spin.

Heats of formation or dissociation. - The heats of formation or dissociation for the molecules considered in this report are given in the following table:

Reaction (all substances in gas phase)	Heat of formation or dissociation, ΔH		Temperature of reaction, $^{\circ}\text{K}$	Reference
	cm^{-1}	cal/mole		
$\text{Q} + \text{H}_2 \rightarrow 2\text{H}$	36,116	103,263	0	5
$\text{Q} + \text{O}_2 \rightarrow 2\text{O}$	41,260	117,971	0	6
$\text{H}_2 + \frac{1}{2} \text{O}_2 \rightarrow \text{H}_2\text{O} + \text{Q}$	-----	57,797.9	298.16	7
$\text{Q} + \text{OH} \rightarrow \text{O} + \text{H}$	35,450	101,359	0	8

Where values are given in centimeter $^{-1}$, they are converted by taking 1 centimeter $^{-1}$ equivalent to 2.85921 calories per mole, calculated from data given in reference 9. The base used in this report for assigning absolute values to enthalpy is the same as in reference 1.

Viscosity data. - Viscosity data are needed for heat-transfer calculations; however, accurate data for gases at high temperatures are unavailable in the literature. Theoretical considerations of force fields lead to theoretical expressions for viscosity that fit available experimental data fairly well and therefore provide a basis upon which experimental data may be extrapolated into the higher temperature regions.

A detailed treatment of the derivation of various theoretical equations for viscosity is given in references 10 and 11. The use of these equations to obtain a refined numerical calculation of viscosity involves the selection of a force-field potential and considerable numerical work. Much of this numerical work can be saved by using tables of collision integrals such as those based on the Lennard-Jones 6-12 potential and the following equation (ref. 11):

$$\mu \times 10^7 = \frac{266.93 \sqrt{T} f_{\mu}^{(k)}}{\sigma_{\Omega}^2 (2,2)^*} \quad (1)$$

The parameters $\Omega^{(2,2)*}$ and $f_{\mu}^{(k)}$ for nonpolar gases are tabulated in reference 11 as a function of reduced temperature T^* while $\Omega^{(2,2)*}$ for polar gases ($f_{\mu}^{(k)}$ assumed to be unity) is tabulated in reference 12 as a function of T^* and δ .

The force constants ϵ/k and σ for H_2 , O_2 , and H and ϵ/k , σ , and δ for H_2O were calculated from experimental viscosity data. No experimental viscosity data were found for O and OH. The value of σ for O was estimated from equations in reference 13, and the value of ϵ/k was taken to be equal to that of O_2 . The values of σ and ϵ/k for OH were estimated from the following equations:

$$\sigma_{OH} = \frac{\sigma_{O_2} + \sigma_{H_2}}{2} \quad (2)$$

$$(\epsilon/k)_{OH} = \sqrt{(\epsilon/k)_{O_2} (\epsilon/k)_{H_2}} \quad (3)$$

The force constants selected are summarized in the following table:

Substance	σ , Å	ϵ/k , °K	δ	Reference
H	2.497	99.8		a ₁₄
H_2	2.729	86.1		a ₂
H_2O	3.487	126.3	2.409	a ₁₅
O	3.068	102.2		b ₁₃
O_2	3.490	102.2		a ₂
OH	3.110	93.8		(c)

^aCalculated from data in reference given.

^bEstimated from equations in reference given and ϵ/k assumed equal to that of O_2 .

^cEstimated by means of equations (2) and (3).

Physical and thermochemical data. - Several physical and thermochemical properties of the propellants are listed in table I. Additional properties of hydrogen may be found in references 16 and 17 while properties of oxygen may be found in reference 18.

FORMULAS

The formulas used in computing the various performance parameters are as follows:

Specific impulse with ambient and exit pressures equal,
(lb force)(sec)/lb mass:

$$I = 294.98 \sqrt{\frac{h_c - h_e}{1000}} \quad (4)$$

Specific impulse in vacuum, (lb force)(sec), lb mass:

$$I_{vac} = I + P \left(\frac{A}{w} \right) \quad (5)$$

Nozzle area per unit mass-flow rate, (sq in)(sec)/lb:

$$\frac{A}{w} = \frac{86.4554 T}{P \cancel{I}} \quad (6)$$

Throat area per unit mass-flow rate, (sq in)(sec)/lb:

$$\frac{A_t}{w} = \frac{2781.6 T_t}{P_t \cancel{I} a} \quad (7)$$

This equation is derived from the continuity equation and the fact that velocity of flow equals velocity of sound at the throat.

Velocity of sound, ft/sec:

$$a = \sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s} = \sqrt{\frac{P}{\rho} \left(\frac{\partial \ln P}{\partial \ln \rho}\right)_s} = 299.16 \sqrt{\left(\frac{T}{\cancel{I}}\right) \left(\frac{\partial \ln P}{\partial \ln \rho}\right)_s} \quad (8)$$

Characteristic velocity, ft/sec:

$$c^* = g_c P_c \frac{A_t}{w} = 32.174 P_c \frac{A_t}{w} \quad (9)$$

Coefficient of thrust:

$$C_F = \frac{gcI}{c^*} = \frac{32.174 I}{c^*} \quad (10)$$

Ratio of nozzle area to throat area

$$\epsilon = \frac{A_w}{A_t w} \quad (11)$$

Partial Derivatives .

The derivatives of the fundamental thermodynamic quantities have many useful applications. Equations (24) to (27) are examples of these applications.

All the relations between first derivatives may be expressed in terms of three arbitrary first derivatives in addition to the fundamental quantities. The three derivatives selected for this report are $(\partial h/\partial T)_P = c_p$, $(\partial \ln M/\partial \ln T)_P$, and $(\partial \ln M/\partial \ln P)_T$. Specific heat c_p is needed in heat-transfer calculations and the other two derivatives are a useful indication of the extent of dissociation.

These derivatives were obtained by means of the following equations:

$$c_p = \frac{1}{PMT} \left[\sum_i p_i (H_T^0)_i \left(\frac{\partial \ln p_i}{\partial \ln T} \right)_P - \mathcal{A} h \left(\frac{\partial \ln \mathcal{A}}{\partial \ln T} \right)_P + T \sum_i p_i (C_P^0)_i \right] \quad (12)$$

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \frac{P}{\sum_i p_i \left(\frac{\partial \ln p_i}{\partial \ln \mathcal{A}} \right)_T} - 1 \quad (13)$$

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P = \left(\frac{\partial \ln \mathcal{A}}{\partial \ln T} \right)_P \quad (14)$$

where $(\partial \ln p_i/\partial \ln T)_P$, $(\partial \ln \mathcal{A}/\partial \ln T)_P$, and $(\partial \ln p_i/\partial \ln \mathcal{A})_T$ are found by matrix methods similar to those described for obtaining $(\partial \ln p_i/\partial \ln T)_S$ in reference 1, and where \mathcal{A} is A in reference 1.

Reference 19 presents a convenient scheme for expressing all first derivatives in terms of $(\partial v/\partial T)_P$, $(\partial v/\partial P)_T$, and $(\partial h/\partial T)_P = c_p$. By means

of the following equations, $(\partial v/\partial T)_P$ and $(\partial v/\partial P)_T$ can be obtained from the derivatives given in this report:

$$\left(\frac{\partial v}{\partial T}\right)_P = - \frac{v}{T} \left[\left(\frac{\partial \ln M}{\partial \ln T} \right)_P - 1 \right] \quad (15)$$

$$\left(\frac{\partial v}{\partial P}\right)_T = - \frac{v}{P} \left[\left(\frac{\partial \ln M}{\partial \ln P} \right)_T + 1 \right] \quad (16)$$

With the aid of the tables in reference 19 and equations (15) and (16), other first derivatives can be expressed in terms of c_p , $(\partial \ln M/\partial \ln T)_P$, and $(\partial \ln M/\partial \ln P)_T$. Some examples are,

$$c_v = c_p - \frac{\alpha}{M} \frac{\left[1 - \left(\frac{\partial \ln M}{\partial \ln T} \right)_P \right]^2}{1 + \left(\frac{\partial \ln M}{\partial \ln P} \right)_T} \quad (17)$$

$$\gamma = \left(\frac{\partial \ln P}{\partial \ln \rho} \right)_S = \frac{c_p}{c_p \left[1 + \left(\frac{\partial \ln M}{\partial \ln P} \right)_T \right] - \frac{\alpha}{M} \left[1 - \left(\frac{\partial \ln M}{\partial \ln T} \right)_P \right]^2} \quad (18)$$

or

$$\gamma = \frac{c_p}{c_v} \left[\frac{1}{1 + \left(\frac{\partial \ln M}{\partial \ln P} \right)_T} \right] \quad (19)$$

When composition is frozen,

$$\left(\frac{\partial \ln M}{\partial \ln P} \right)_T = \left(\frac{\partial \ln M}{\partial \ln T} \right)_P = 0 \quad (20)$$

and equations (17) and (18) reduce to

$$c_v = c_p - \frac{\alpha}{M}$$

and

$$\gamma = \frac{c_p}{c_p - \frac{\alpha}{M}} = \frac{c_p}{c_v} \quad (21)$$

Viscosity of Mixtures

Viscosities of multicomponent mixtures calculated by rigorous methods (refs. 11 and 20) show excellent agreement with experimental data. However, these calculations involve considerable effort and become increasingly more difficult with increasing number of components. Simpler techniques, but which still involve considerable calculations, are given in references 21 and 22.

The following equation, based on averaging kinematic viscosities, gives approximate results, which are often sufficiently accurate for engineering purposes:

$$\mu = \frac{\mathcal{M}}{\sum_i \frac{x_i \mathcal{M}_i}{\mu_i}} \quad (22)$$

The equation appears adequate until better high-temperature data for the individual components become available.

Conductivity

Thermal conductivities as well as viscosities are needed in heat-transfer calculations. However, experimental conductivity data are generally even less available than experimental viscosity data. Therefore, the Eucken relation

$$k = \mu \left(c_p + \frac{5}{4} \frac{\mathcal{R}}{\mathcal{M}} \right) \quad (23)$$

which often gives satisfactory values of conductivity for individual components, is used in this report to estimate the conductivity of gaseous mixtures.

THEORETICAL PERFORMANCE DATA

Tables

The calculated values of the various performance parameters for combustion pressures of 60, 150, 300, and 600 pounds per square inch absolute and for a range of equivalence ratios and exit conditions are given in tables II to V. Table II presents performance data at assigned pressure ratios from 1 to 4000 for equivalence ratios from 0.15 to 5.00 (oxidant-fuel weight ratios from 1.190 to 39.683). Properties at the throat may be found where $\epsilon = 1.00$. Table III gives various thermodynamic partial

derivatives. Equilibrium composition in the combustion chamber and at the assigned exit conditions is given in table IV. Characteristic velocity and summary of the performance parameters at an exit pressure of 1 atmosphere are presented in table V.

Curves

The performance parameters are plotted in figures 1 to 8. Curves of specific impulse are presented in figure 1 for assigned pressure ratios as functions of percent by weight of fuel. Combustion temperature and exit temperature for assigned pressure ratios are plotted in figure 2 as functions of percent by weight of fuel. Curves of the ratio of nozzle area to throat area are plotted in figure 3 as functions of percent by weight of fuel for assigned pressure ratios. Figure 4 gives the curves for coefficient of thrust for assigned pressure ratios as functions of percent by weight of fuel; figure 5 presents curves of molecular weight for assigned pressure ratios; and figure 6 presents curves of characteristic velocity as functions of percent by weight of fuel. Figure 7 gives curves of specific impulse in vacuum for assigned area ratios as functions of percent by weight of fuel. The curves of figure 7 were obtained by interpolation of the data at assigned pressure ratios.

Effect of Assuming Frozen or Equilibrium Composition During Expansion

A comparison of specific impulse data based on equilibrium and frozen composition during expansion to an exit pressure of 1 atmosphere is given in figure 8. A comparison of maximum calculated values of specific impulse based on equilibrium and frozen composition during expansion is shown in the following table for expansion to 1 atmosphere and to pressure ratios of 100 and 4000 (taken from table II):

Chamber pressure, P_c , lb/sq in. abs	Pressure ratio, P_c/P	Equivalence ratio, R, at which I is maximum	Oxidant-fuel weight ratio, O/F	Composition during expansion	Maximum specific impulse, I, (lb)(sec) lb	Difference in I, percent
60	4.083	0.35	2.778	Equilibrium	255.4	0.31
		.35	2.778	Frozen	254.6	
		100	0.45	Equilibrium	400.8	1.67
	4000	.40	3.571	Frozen	394.2	
		0.70	3.175	Equilibrium	465.9	3.81
		.40	3.175	Frozen	448.8	
	10.207	0.40	3.175	Equilibrium	315.0	0.61
		.35	2.778	Frozen	313.1	
		100	0.50	Equilibrium	401.3	1.42
150		.40	3.968	Frozen	395.7	
4000	0.70	5.556	Equilibrium	466.6	3.37	
	.45	3.571	Frozen	451.4		
	20.414	0.45	Equilibrium	348.1	0.67	
300	.40	3.571	Frozen	345.8		
	100	0.50	Equilibrium	401.5	1.24	
	.40	3.175	Frozen	396.6		
4000	0.70	5.556	Equilibrium	467.0	3.02	
	.45	3.571	Frozen	453.3		
600	40.827	0.50	3.968	Equilibrium	374.5	0.73
		.40	3.175	Frozen	371.8	
		100	0.50	Equilibrium	401.7	1.06
	4000	.45	3.571	Frozen	397.5	
		0.70	5.556	Equilibrium	467.4	2.75
		.50	3.968	Frozen	454.9	

The preceding table shows that for pressure ratios up to 100, the difference in maximum specific impulse due to equilibrium or frozen composition during expansion is less than 2 percent. For a pressure ratio of 4000 the difference increases to 3 to 4 percent. However, the maximum specific impulse occurs in general at a higher oxidant-fuel ratio O/F for equilibrium composition than for frozen composition.

A comparison of values of specific impulse for frozen and equilibrium composition at the same O/F could show larger differences. For example, from data in table II, for a chamber pressure of 60 pounds per square inch

absolute, a pressure ratio of 4000, an O/F of 5.556 (where equilibrium specific impulse is maximum) the difference in specific impulse for frozen and equilibrium composition is 9.6 percent. For the same conditions but for the stoichiometric O/F of 7.937, the difference is 15.8 percent. This is the largest difference between frozen and equilibrium specific impulse at constant O/F for any of the conditions in this report.

The O/F for maximum specific impulse increases with increasing pressure ratio. For fixed pressure ratios and frozen composition the O/F for maximum specific impulse increases with increasing chamber pressure.

Effect of Chamber Pressure

By use of suitable exponents, performance parameters can be estimated with good accuracy at chamber pressures other than those given in this report. The logarithmic values of the parameters I , I_{vac} , T , ϵ , and c^* are very nearly linear with the logarithm of chamber pressure for a fixed equivalence ratio and pressure ratio or fixed equivalence ratio and area ratio. This linearity permits the data to be extended by means of exponential equations.

In the case of equilibrium composition, the following analytic expressions were derived that permit the exponents to be computed from data at a single chamber pressure:

$$n_I = \left(\frac{\partial \ln I}{\partial \ln P_c} \right)_{P_c/P} = 86.4554 \frac{T}{I^2} \left(\frac{1}{M_c} - \frac{1}{M} \right) \quad (24)$$

$$n_T = \left(\frac{\partial \ln T}{\partial \ln P_c} \right)_{P_c/P} = \frac{\gamma}{M_p c_p} \left[1 - \left(\frac{\partial \ln M}{\partial \ln T} \right)_P \right] - \frac{\gamma}{c_p M_c} \quad (25)$$

$$n_\epsilon = \left(\frac{\partial \ln \epsilon}{\partial \ln P_c} \right)_{P_c/P} = (n_{A/w})_e - (n_{A/w})_t \quad (26)$$

where

$$n_{A/w} = \left(\frac{\partial \ln A/w}{\partial \ln P_c} \right)_{P_c/P} = - \frac{\gamma}{c_p M_c} \left[1 - \left(\frac{c}{c} \frac{\ln M}{\ln T} \right)_P \right] - \frac{1}{r} - n_I$$

$$n_{c^*} = \frac{\partial \ln c^*}{\partial \ln P_c} = 1 + (n_{A/w})_t \quad (27)$$

$$n_{I_{vac}} = \left(\frac{\partial \ln I_{vac}}{\partial \ln P_c} \right)_{P_c/P} = \frac{I(n_I - n_{c^*} - n_\epsilon)}{I_{vac}} + n_{c^*} + n_\epsilon \quad (28)$$

Equations (24) to (28) may be written in the approximate form:

$$I = I_l \left(\frac{P_c}{P_{c,l}} \right)^{n_{I,l}} \quad (29)$$

$$T = T_l \left(\frac{P_c}{P_{c,l}} \right)^{n_{T,l}} \quad (30)$$

$$\epsilon = \epsilon_l \left(\frac{P_c}{P_{c,l}} \right)^{n_{\epsilon,l}} \quad (31)$$

$$c^* = c_l^* \left(\frac{P_c}{P_{c,l}} \right)^{n_{c^*,l}} \quad (32)$$

$$I_{vac} = I_{vac,l} \left(\frac{P_c}{P_{c,l}} \right)^{n_{I_{vac},l}} \quad (33)$$

where $P_{c,l}$ may be either 60, 150, 300, or 600 pounds per square inch absolute provided that I_l , T_l , ϵ_l , c_l^* , $I_{vac,l}$, and their derivatives are the corresponding values for the chamber pressure selected.

The exponents obtained by means of equations (24) to (28) are shown in table III.

In order to illustrate the use of these derivatives, suppose it is desired to obtain the value of equilibrium specific impulse for a chamber pressure of 1200 pounds per square inch absolute and a pressure ratio of 81.65 (exit pressure, 1 atm) for an equivalence ratio R of 0.90 ($O/F = 7.143$): From table III, the value of I at this pressure ratio and equivalence ratio (but for a chamber pressure of 600 lb/sq in. abs) is 376.8 and the value of n_I is 0.0079. From equation (29),

$$I = 376.8 \left(\frac{1200}{600} \right)^{0.0079}$$

$$= 376.8(1.0055)$$

$$= 378.9$$

A comparison of the parameters obtained by means of the chamber-pressure correlation and by a direct calculation is given in the following table ($R = 0.90$, equilibrium composition during expansion):

Parameter	Chamber pressure, P_c , 1200 lb/sq in. abs;		
	Estimated by corre- lation	Direct calcu- lation	Error
I	378.93	378.86	0.07
T_c	3623.3	3622.0	1.3
T_e	2338.4	2338.6	.2
ϵ	11.769	11.755	.014
c^*	7306.1	7304.7	1.4

It is expected that values estimated for other equivalence ratios and pressure ratios for chamber pressures from about 30 to 1200 pounds per square inch absolute will have small errors of the order of magnitude shown in the previous table.

The following analytic expressions were derived for equilibrium composition which permit exponents to be computed similar to those in equations (24) to (28) but for constant area ratio rather than constant pressure ratio (eqs. 34, 37, 38, 40):

$$\left(\frac{\partial \ln P_c/P}{\partial \ln P_c} \right)_\epsilon = n_\epsilon / \left(\frac{\partial \ln \epsilon}{\partial \ln P} \right)_s \quad (34)$$

where

$$\left(\frac{\partial \ln \epsilon}{\partial \ln P}\right)_s = -\frac{1}{\gamma} - \left(\frac{\partial \ln I}{\partial \ln P}\right)_s \quad (35)$$

and

$$\left(\frac{\partial \ln I}{\partial \ln P}\right)_s = -86.4554 \frac{T}{I^2} \text{ or } 1 - \frac{I_{vac}}{I} \quad (36)$$

$$\left(\frac{\partial \ln I}{\partial \ln P_c}\right)_\epsilon = n_I - \left(\frac{\partial \ln I}{\partial \ln P}\right)_s \left(\frac{\partial \ln P_c/P}{\partial \ln P_c}\right)_\epsilon \quad (37)$$

$$\left(\frac{\partial \ln T}{\partial \ln P_c}\right)_\epsilon = n_T - \left(\frac{\partial \ln T}{\partial \ln P}\right)_s \left(\frac{\partial \ln P_c/P}{\partial \ln P_c}\right)_\epsilon \quad (38)$$

where

$$\left(\frac{\partial \ln T}{\partial \ln P}\right)_s = \frac{A}{M c_p} \left[1 - \left(\frac{\partial \ln A}{\partial \ln T}\right)_P \right] \quad (39)$$

$$\left(\frac{\partial \ln I_{vac}}{\partial \ln P_c}\right)_\epsilon = n_{I_{vac}} - \left(\frac{\partial \ln I_{vac}}{\partial \ln P}\right)_s \left(\frac{\partial \ln P_c/P}{\partial \ln P_c}\right)_\epsilon \quad (40)$$

$$= \frac{I(n_I - n_{c*})}{I_{vac}} + n_{c*}$$

where

$$\left(\frac{\partial \ln I_{vac}}{\partial \ln P}\right)_s = \left(\frac{\partial \ln \epsilon}{\partial \ln P}\right)_s \left(1 - \frac{I}{I_{vac}}\right) \quad (41)$$

Data for constant area ratios for chamber pressures other than those given in this report may be obtained in a manner similar to the previous example by interpolating the data in table II (see, for example, fig. 7) together with exponents obtained from equations (34) to (41).

Effect of Finite Chamber Area

The use of a combustion chamber of finite cross-sectional area leads to a pressure change during the combustion process. For a cylindrical

chamber, the injector face pressure P_{in} may be found from the following equation derived from the conservation of the momentum

$$P_{in} = P_1 + \frac{w}{A_1 g_c} (V_1 - V_{in}) \quad (42)$$

where P_1 and V_1 are the static pressure and velocity at the nozzle entrance, respectively, and V_{in} is the average velocity of propellant (liquid or gas) in the axial direction when injected. Equation (42) may be written

$$P_{in} = P_c \left(\frac{P_1}{P_c} \right) (I_1 g_c - V_{in}) \quad (43)$$

where P_c is the stagnation pressure in the nozzle.

In order to illustrate this, consider a rocket operating at an equivalence ratio of 1.00, a nozzle stagnation pressure of 600 pounds per square inch absolute, a ratio of chamber area to throat area ϵ of 2.122, and $V_{in} = 100$ feet per second. From table II, corresponding to an area ratio of 2.122, P_c/P_1 is 1.05 and I is 43.3. From table V, c^* is 7039. Therefore, for these conditions, using equation (43),

$$\begin{aligned} P_{in} &= 600 \left(\frac{1}{1.05} \right) + \frac{600}{7039(2.122)} [(43.3)(32.17) - 100] \\ &= 571.4 + 51.9 \\ &= 623.3 \text{ lb/sq in. abs} \end{aligned}$$

SUMMARY OF RESULTS

A theoretical investigation of the performance of liquid hydrogen with liquid oxygen was made for the following conditions: (1) equilibrium and frozen composition during expansion, (2) four chamber pressures (60, 150, 300, and 600 lb/sq in. abs), (3) wide range of oxidant-fuel weight ratios (1.190 to 39.683), and (4) wide range of pressure ratios (1 to 4000).

1. The maximum values of specific impulse for expansion to 1 atmosphere are summarized in the following table:

Chamber pressure, P_c , lb/sq in. abs	Ratio of chamber pressure to exit pressure, P_c/P	Specific impulse, I, (lb)(sec)/lb	
		Equilibrium composition	Frozen composition
60	4.083	255.4	254.6
150	10.207	315.0	313.1
300	20.414	348.1	345.8
600	40.827	374.5	371.8

The maximum value of specific impulse for a chamber pressure of 600 pounds per square inch absolute and a pressure ratio of 4000 is 467.4 and 454.9 assuming equilibrium and frozen composition, respectively.

2. The difference between maximum values of specific impulse due to the assumption of equilibrium or frozen composition during expansion is less than 2 percent for pressure ratios up to 100 and about 3 to 4 percent for a pressure ratio of 4000.

3. For the same oxidant-fuel ratios, the difference between values of specific impulse due to the assumption of equilibrium or frozen composition during expansion may be as high as 15.8 percent for the conditions in this report.

Lewis Research Center

National Aeronautics and Space Administration
Cleveland, Ohio, March 2, 1959

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TABLE I. - PROPERTIES OF LIQUID PROPELLANTS

Properties	Hydrogen	Oxygen
Molecular weight, \mathcal{M}	2.016	32.00
Density, g/cc	^a 0.0709 (at -252.7° C)	^b 1.1414 (at -182.0° C)
Freezing point, °C	^c -259.20	^c -218.76
Boiling point, °C	^c -252.77	^c -182.97
Enthalpy required to convert liquid at boiling point to gaseous elements at 25° C, kcal/mole	^d 1.894	^d 3.081
Enthalpy of vaporization, kcal/mole	^c 0.216 (at -252.77° C)	^c 1.630 (at -182.97° C)
Enthalpy of fusion, kcal/mole	^c 0.028 (at -259.20° C)	^c 0.106 (at -218.76° C)

^aRef. 23.^bRef. 24.^cRef. 7.^dRef. 1.

TABLE II. - THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

(Equivalence ratio, R; oxidant-fuel ratio, O/F.)

(a) Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb/in ² abs	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K/cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/sec/lb	Area ratio, E	Thrust coefficient, C_F	Specific impulse, I , lb/sec/lb
$R = 0.150$, PERCENT FUEL = 45.65%, O/F = 1.190													
1.00	60.00	1183	2313.5	4.416	1.3595	1.7753	514	0.00073	0.000			0.000	0.0
1.05	57.14	1186	2287.7	4.416	1.3400	1.7711	511	0.00073	271	250.1	2.250	210	474.4
1.20	50.00	1129	2118.6	4.416	1.3400	1.7757	303	0.00070	267	234.6	1.297	403	90.8
1.40	42.86	1085	2141.6	4.416	1.3409	1.7472	293	0.00068	272	296.1	1.081	543	122.2
1.60	37.50	1049	2077.7	4.416	1.3447	1.7369	285	0.00066	860	286.6	1.018	636	143.2
1.87	32.17	1006	2008.6	4.416	1.3502	1.7257	276	0.00063	1.000	244.1	1.000	725	163.4
2.00	30.00	989	1975.4	4.416	1.3520	1.7120	274	0.00062	1.059	244.4	1.001	761	171.5
4.00	15.00	824	4693.4	4.416	1.3551	1.6625	234	0.00052	1.556	301.7	1.233	1.031	234.3
4.08	14.70	819	4682.8	4.416	1.3554	1.65510	232	0.00052	1.579	302.3	1.244	1.038	233.7
10.00	6.00	643	4392.5	4.416	1.3748	1.6507	180	0.00042	2.152	327.5	1.974	1.257	483.1
20.00	3.00	552	4209.8	4.416	1.3600	1.6345	159	0.00035	2.086	343.5	1.983	1.176	309.9
40.00	1.50	439	4058.9	4.416	1.3584	1.6200	153	0.00029	3.031	356.4	4.620	1.067	330.4
100.00	.60	340	3895.0	4.416	1.3800	1.6099	104	0.00023	3.646	369.8	8.432	1.058	350.8
200.00	.30	280	3802.6	4.416	1.3930	1.5951	85	0.00018	4.148	377.7	13.431	1.010	362.6
400.00	.15	230	3723.2	4.416	1.4064	1.5573	70	0.00015	4.615	384.1	21.488	1.052	372.0
1000.00	.06	175	3640.1	4.416	1.43359	1.44871	52	0.00011	2.440	390.6	39.928	1.094	381.6
2000.00	.03	142	3590.9	4.416	1.43544	1.4402	43	0.00009	6.098	394.3	63.572	1.071	387.2
4000.00	.02	114	3551.2	4.416	1.44680	1.44116	36	0.00007	6.851	357.3	100.939	1.0739	391.6
$R = 0.200$, PERCENT FUEL = 38.65%, O/F = 1.587													
1.00	60.00	1514	2969.7	5.216	1.3077	1.6194	404	0.00084	0.000			0.000	0.0
1.02	57.14	1497	2941.7	5.216	1.3080	1.6194	399	0.00083	274	254.1	2.233	209	494.3
1.20	50.00	1450	2868.6	5.216	1.3119	1.6028	389	0.00081	553	348.6	1.289	400	94.6
1.40	42.86	1399	2785.1	5.216	1.3124	1.5891	378	0.00078	730	307.3	1.077	529	147.4
1.60	37.50	1354	2713.2	5.216	1.3184	1.5774	369	0.00075	869	299.6	1.016	632	149.4
1.83	32.44	1307	2640.5	5.216	1.3217	1.5639	359	0.00073	1.000	247.3	1.000	716	169.2
2.00	30.00	1282	2601.1	5.216	1.3235	1.5559	353	0.00072	1.038	297.8	1.004	757	179.1
4.00	15.00	1079	2290.0	5.216	1.3391	1.5046	307	0.00061	1.572	316.7	1.244	1.029	243.2
4.08	14.70	1073	2281.6	5.216	1.3395	1.5031	306	0.00061	1.595	317.4	1.256	1.033	244.7
10.00	6.00	852	1954.3	5.216	1.3559	1.4516	251	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	3.00	709	1748.8	5.216	1.3506	1.4423	213	0.00040	2.573	362.0	3.049	1.379	325.9
40.00	1.50	568	1570.0	5.216	1.3714	1.4057	179	0.00034	3.010	376.0	4.759	1.472	348.0
100.00	.60	428	1396.5	5.216	1.3770	1.3916	146	0.00026	3.619	390.5	8.679	1.065	370.0
200.00	.30	372	1286.1	5.216	1.3811	1.3900	117	0.00022	4.111	397.1	15.070	1.019	396.7
400.00	.15	312	1190.2	5.216	1.3929	1.3501	96	0.00018	4.638	405.0	22.249	1.064	395.0
1000.00	.06	242	1098.9	5.216	1.3973	1.3370	74	0.00013	5.374	412.4	41.979	1.076	405.5
2000.00	.03	198	1041.1	5.216	1.4144	1.2794	61	0.00011	6.312	411.7	67.657	1.073	409.7
4000.00	.02	161	993.9	5.216	1.4352	1.2204	50	0.00009	6.704	421.1	108.755	1.0754	414.6
$R = 0.250$, PERCENT FUEL = 32.51%, O/F = 1.984													
1.00	60.00	1816	1249.3	6.015	1.2812	1.5080	481	0.00092	0.000			0.000	0.0
1.05	57.14	1797	1220.2	6.016	1.2824	1.5036	477	0.00091	277	563.4	2.218	207	50.3
1.20	50.00	1744	1142.1	6.016	1.2822	1.4958	467	0.00089	258	559.4	1.483	358	96.6
1.40	42.86	1686	1054.8	6.016	1.2809	1.4751	456	0.00086	236	516.3	1.073	556	130.1
1.60	37.50	1636	981.5	6.016	1.2919	1.4630	446	0.00084	287	508.0	1.019	629	152.0
1.83	32.78	1587	910.0	6.016	1.2948	1.4513	436	0.00081	1.000	504.2	1.000	708	171.8
2.00	30.00	1555	864.0	6.016	1.2998	1.4436	429	0.00080	1.076	503.1	1.005	754	163.1
4.00	15.00	1382	535.1	6.016	1.3263	1.3817	378	0.00068	1.575	525.2	1.226	1.026	249.3
4.08	14.70	1316	526.2	6.016	1.3319	1.3860	377	0.00068	1.592	526.2	1.238	1.033	250.8
10.00	6.00	1057	176.1	6.016	1.3526	1.3226	314	0.00024	2.147	352.3	2.048	1.258	305.6
20.00	3.00	887	995.0	6.016	1.3401	1.2848	269	0.00016	2.563	373.7	3.127	1.382	335.7
40.00	1.50	741	766.1	6.016	1.3569	1.2559	228	0.00008	2.987	388.7	4.883	1.478	359.0
100.00	.60	581	569.1	6.016	1.3663	1.2521	181	0.00030	3.581	404.2	8.985	1.074	382.4
200.00	.30	482	4947.8	6.016	1.3717	1.2170	151	0.00025	4.063	413.4	14.596	1.630	395.9
400.00	.15	399	474.7	6.016	1.3752	1.2100	129	0.00020	4.581	420.7	23.200	1.675	408.8
1000.00	.06	310	9240.5	6.016	1.3926	1.1943	97	0.00012	5.321	426.7	43.894	1.721	418.1
2000.00	.03	296	9175.9	6.016	1.3880	1.1603	76	0.00012	5.745	429.4	71.279	1.749	426.7
4000.00	.02	210	9122.7	6.016	1.4031	1.1441	64	0.00010	6.606	437.2	115.670	1.771	430.2
$R = 0.300$, PERCENT FUEL = 29.57%, O/F = 2.031													
1.00	60.00	2089	9932.7	6.812	1.2220	1.4578	520	0.00100	0.000			0.000	0.0
1.05	57.14	2069	9904.2	6.812	1.2264	1.4493	526	0.00099	279	568.2	2.204	206	50.7
1.20	50.00	2015	9823.7	6.812	1.2313	1.4276	526	0.00096	543	557.6	1.277	395	97.4
1.40	42.86	1930	9734.6	6.814	1.2644	1.4024	522	0.00093	742	518.7	1.070	533	131.3
1.60	37.50	1856	9659.7	6.815	1.2679	1.3879	513	0.00090	883	510.2	1.013	629	154.1
1.83	33.04	1846	9590.7	6.815	1.2711	1.3724	503	0.00086	1.000	504.2	1.000	700	174.5
2.00	30.00	1808	9539.4	6.815	1.2754	1.3623	488	0.00085	1.083	507.0	1.050	624.5	152.1
4.00	15.00	1593	9200.0	6.816	1.2870	1.3008	449	0.00074	1.585	530.2	1.204	1.024	224.5
4.08	14.70	1546	9190.8	6.816	1.2879	1.2974	443	0.00074	1.598	531.3	1.215	1.031	234.1
10.00	6.00	1220	5825.6	6.816	1.3074	1.2557	375	0.00060	2.148	361.8	2.085	1.259	310.4
20.00	3.00	1084	5071.4	6.816	1.3240	1.2071	322	0.00051	2.522	381.4	3.201	1.306	341.6
40.00	1.50	896	5075.3	6.816	1.3330	1.1751	279	0.00042	2.768	397.0	5.036	1.485	365.9
100.00	.60	704	8180.5	6.816	1.3320	1.1174	223	0.00033	3.543	413.2	9.326	1.584	370.5
200.00	.30	270	8049.4	6.816	1.3304	1.1003	197	0.00027	4.013	425.3	14.595	1.604	374.8
400.00	.15	490	7940.7	6.816	1.3305	1.0961	156	0.00023	4.516				

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P_e in abs.	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec·°K·cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb/sec)/lb	Area ratio, E	Thrust coefficient, C_t , lb-force/lb	Specific impulse, I , lb-force/lb
$R = 0.350$; PERCENT FUEL = 26.47; O/F = 2.778													
1.00	60.00	2329	8892.8	7.597	1.2267	1.4897	608	0.0010	0.000	568.4	2.189	0.000	0.0
1.05	57.14	2309	8863.2	7.597	1.2284	1.4752	605	0.0009	.282	360.3	1.270	.393	50.7
1.20	50.00	2253	8783.6	7.602	1.2330	1.4382	595	0.0005	.548	360.3	1.067	.530	97.5
1.40	42.86	2189	8694.1	7.606	1.2302	1.3999	585	0.0001	.749	320.7	1.012	.622	131.5
1.60	37.50	2133	8618.7	7.608	1.2425	1.3707	575	0.0098	.890	311.6	1.012	.622	154.4
1.80	33.32	2085	8553.6	7.610	1.2462	1.3475	566	0.0095	1.000	309.7	1.000	.692	171.8
2.00	30.00	2042	8497.1	7.611	1.2494	1.3289	559	0.0092	1.090	310.6	1.007	.747	185.6
4.00	15.00	1772	8152.4	7.615	1.2679	1.2591	506	0.0079	1.589	333.1	1.277	1.022	253.8
4.00	14.70	1764	8145.0	7.615	1.2684	1.2571	504	0.0079	1.603	333.8	1.289	1.029	255.4
10.00	6.00	1452	7768.0	7.616	1.2882	1.1665	434	0.0065	2.147	365.5	2.121	1.260	312.8
20.00	3.00	1239	7528.0	7.616	1.3035	1.1208	381	0.0055	2.248	385.8	3.285	1.389	345.0
40.00	1.50	1051	7318.3	7.616	1.3167	1.0795	330	0.0046	2.951	402.4	5.194	1.491	370.1
100.00	.60	838	7093.2	7.616	1.3364	1.0566	268	0.0036	3.509	419.6	9.687	1.594	395.7
200.00	.30	703	6954.1	7.616	1.3374	1.0120	226	0.0030	3.962	430.1	15.643	1.654	410.7
400.00	.15	587	6837.8	7.616	1.3552	.9924	189	0.0025	4.651	438.6	25.377	1.703	422.9
1000.00	.06	460	6713.2	7.616	1.3654	.9790	148	0.0019	5.159	447.5	48.339	1.754	435.5
2000.00	.03	382	6637.2	7.616	1.3683	.9694	121	0.0016	5.748	452.8	78.934	1.784	443.0
4000.00	.02	317	6574.1	7.616	1.3733	.9600	98	0.0013	6.389	457.2	129.082	1.809	449.2
$R = 0.400$; PERCENT FUEL = 23.95; O/F = 3.175													
1.00	60.00	2331	8050.5	8.363	1.1996	1.6075	655	0.0025	0.000	565.1	2.173	.203	50.4
1.05	57.14	2312	8021.3	8.366	1.2011	1.5870	655	0.0023	.266	565.1	1.263	.390	96.9
1.20	50.00	2456	7942.5	8.374	1.2025	1.5554	645	0.0018	.554	358.7	1.063	.526	130.8
1.40	42.86	2396	7855.8	8.383	1.2107	1.4758	635	0.0013	.756	319.7	1.010	.618	153.8
1.60	37.50	2342	7778.0	8.389	1.2123	1.4500	626	0.0008	.898	310.8	1.000	.683	169.9
1.75	33.62	2298	7711.0	8.393	1.2142	1.3954	619	0.0005	1.000	309.4	1.008	.744	184.9
2.00	30.00	2252	7657.4	8.397	1.2222	1.3620	611	0.0001	1.098	310.3	1.008	.744	184.9
4.00	15.00	1978	7311.0	8.411	1.2458	1.2147	561	0.0085	1.594	333.8	1.289	1.020	253.7
4.00	14.70	1970	7301.4	8.411	1.2464	1.2116	559	0.0084	1.607	334.6	1.302	1.027	255.3
10.00	6.00	1840	6920.2	8.416	1.2689	1.1161	490	0.0069	2.145	367.3	2.160	1.261	313.6
20.00	3.00	1411	6670.9	8.416	1.2839	1.0681	435	0.0059	2.540	388.3	3.365	1.393	346.5
40.00	1.50	1207	6457.0	8.416	1.2990	1.0259	381	0.0050	2.934	405.7	5.356	1.497	372.4
100.00	.60	972	6222.0	8.416	1.3100	.9772	313	0.0040	3.476	423.9	10.058	1.604	398.9
200.00	.30	820	6075.6	8.416	1.3316	.9481	266	0.0033	3.914	434.9	16.345	1.667	414.5
400.00	.15	689	5952.4	8.416	1.3420	.9252	224	0.0027	4.384	443.8	26.628	1.718	427.3
1000.00	.06	543	5819.7	8.416	1.3550	.9041	176	0.0021	5.068	453.3	50.955	1.772	440.6
2000.00	.03	453	5736.3	8.416	1.3575	.8830	146	0.0017	5.640	458.9	83.421	1.804	448.5
4000.00	.02	377	5670.6	8.416	1.3646	.8834	119	0.0014	6.262	463.6	130.777	1.830	455.1
$R = 0.450$; PERCENT FUEL = 21.87; O/F = 3.571													
1.00	60.00	2696	7354.5	9.102	1.1774	1.7899	696	0.0044	0.000	559.4	2.159	0.000	0.0
1.05	57.14	2678	7325.9	9.107	1.1785	1.7644	693	0.0041	.288	559.4	2.021	.49.9	
1.20	50.00	2628	7246.6	9.121	1.1819	1.6982	686	0.0035	.559	355.5	1.257	.387	96.0
1.40	42.86	2586	7161.4	9.136	1.1862	1.6247	677	0.0028	.763	317.2	1.080	.523	129.6
1.60	37.50	2519	7078.6	9.148	1.1901	1.5642	669	0.0023	.905	308.6	1.009	.615	152.4
1.75	33.62	2494	7033.2	9.156	1.1923	1.5208	663	0.0019	1.000	307.3	1.000	.675	167.2
2.00	30.00	2454	6967.6	9.164	1.1972	1.4702	655	0.0014	1.107	308.6	1.010	.740	183.5
4.00	15.00	2167	6622.5	9.199	1.2215	1.2440	609	0.0092	1.600	333.1	1.303	1.018	252.4
4.00	14.70	2159	6613.0	9.199	1.2222	1.2389	608	0.0092	1.613	333.9	1.316	1.025	254.0
10.00	6.00	1822	6228.5	9.214	1.2498	1.0871	541	0.0073	2.141	367.6	2.204	1.263	313.0
20.00	3.00	1561	5974.4	9.216	1.2558	1.0282	486	0.0063	2.529	389.3	3.454	1.398	346.5
40.00	1.50	1362	5754.8	9.216	1.2606	.9843	431	0.0054	2.916	407.3	5.529	1.506	373.1
100.00	.60	1109	5511.3	9.216	1.3004	.9335	360	0.0043	3.444	426.6	10.479	1.616	400.5
200.00	.30	594	5356.4	9.216	1.3148	.9005	309	0.0036	3.867	438.0	17.107	1.682	416.8
400.00	.15	796	5228.8	9.216	1.3278	.8733	262	0.0030	4.320	447.4	28.011	1.735	430.1
1000.00	.06	632	5080.3	9.216	1.3415	.8469	208	0.0023	4.979	457.4	53.887	1.792	444.1
2000.00	.03	529	5001.7	9.216	1.3500	.8317	173	0.0019	5.528	463.4	88.516	1.826	452.5
4000.00	.02	441	4929.4	9.216	1.3561	.8212	143	0.0016	6.130	468.4	145.512	1.854	459.4
$R = 0.500$; PERCENT FUEL = 20.12; O/F = 3.968													
1.00	60.00	2828	6769.6	9.611	1.1605	2.0170	728	0.0065	0.000	552.0	2.147	0.000	0.0
1.05	57.14	2811	6741.8	9.619	1.1615	1.9891	725	0.0063	.290	552.0	2.020	.49.2	
1.20	50.00	2765	6665.0	9.639	1.1636	1.9138	719	0.0056	.563	351.2	1.251	.385	94.7
1.40	42.86	2711	6581.4	9.681	1.1667	1.8287	711	0.0048	.769	313.7	1.057	.520	128.0
1.60	37.50	2664	6507.1	9.679	1.1695	1.7571	704	0.0041	.912	305.4	1.008	.612	150.6
1.75	34.19	2632	6554.9	9.690	1.1717	1.7087	696	0.0037	1.000	304.3	1.000	.666	164.2
2.00	30.00	2585	6391.4	9.696	1.1750	1.6426	692	0.0031	1.114	305.8	1.012	.738	181.4
4.00	15.00	2335	6050.4	9.769	1.1964	1.3401	651	0.0003	1.607	331.1	1.317	1.017	250.2
4.00	14.70	2327	6040.9	9.7670	1.1971	1.3326	650	0.0003	1.620	332.0	1.331	1.024	251.8
10.00	6.00	1996	5650.8	10.006	1.2285	1.0939	588	0.0079	2.139	366.7	2.252	1.266	311.3
20.00	3.00	1748	5390.4	10.014	1.2401	1.0036	522	0.0067	2.517	389.1	3.592	1.405	345.4
40.00	1.50	1518	5174.1	10.016	1.2634	.9523	479	0.0058	2.896	407.8	5.719	1.515	372.6
100.00	.60	1247	4923.4	10.016	1.2627	.9003	406	0.0047	3.411	427.7	10.920	1.630	400.8
200.00	.30	1067	4764.5	10.016	1.2676	.8650	352	0.0039	3.821	439.7	17.932	1.698	417.7
400.00	.15	907	4629.0	10.016	1.3118	.8547	304	0.0033	4.258	449.7	29.520	1.755	

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P/P	Static pressure, P, lb/sq.in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p, cal/(g·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/sec·°K/cm	Mach number, M	Specific impulse in vacuum, I_vac, sec	Area ratio, E	Thrust coefficient, C_t, lb/sec./lb	Specific impulse, I, lb.sec./lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	60.00	3015	5841.6	11.142	1.1386	2.5641	771	0.00219	0.000	2.131	1.199	47.7	0.0
1.05	57.14	3001	5815.4	11.155	1.1389	2.5545	775	0.00214	0.293	2.352	2.131	1.199	47.7
1.20	50.00	2961	5744.6	11.186	1.1370	2.4922	769	0.00209	0.691	3.10	1.244	3.84	91.9
1.40	42.86	2914	5664.3	11.221	1.1407	2.3566	764	0.00197	0.776	3.05	1.054	5.17	124.2
1.60	37.50	2874	5596.0	11.251	1.1419	2.2736	757	0.00189	0.921	2.97	1.006	6.09	146.2
1.74	34.45	2849	5554.5	11.269	1.1427	2.2222	753	0.00184	1.000	2.95	1.000	6.65	158.0
2.00	30.00	2807	5484.3	11.299	1.1442	2.1550	747	0.00176	1.125	2.98	1.014	7.56	176.3
4.00	15.00	2595	5156.9	11.429	1.1523	1.7214	719	0.00139	1.621	3.24	1.339	1.016	244.1
4.08	14.70	2588	5147.7	11.432	1.1528	1.7094	714	0.00138	1.634	3.20	1.354	1.023	245.7
10.00	6.00	2249	4768.9	11.547	1.1811	1.2736	665	0.00095	2.143	3.61	2.366	1.272	305.5
20.00	3.00	2063	4509.2	11.593	1.2063	1.027	620	0.00079	2.499	2.85	3.762	1.417	340.5
40.00	1.50	1825	4278.5	11.610	1.2290	0.9310	564	0.00065	4.054	4.05	6.136	1.535	368.8
100.00	.60	1529	4016.0	11.616	1.2505	0.8551	496	0.00053	3.341	4.27	11.885	1.659	398.6
200.00	.30	1326	3846.9	11.616	1.2647	0.8176	440	0.00045	3.728	4.40	19.729	1.734	416.6
400.00	.15	1144	3700.6	11.616	1.2790	0.7842	385	0.00038	4.156	4.51	32.844	1.797	431.6
1000.00	.06	932	3538.3	11.616	1.2981	0.7449	317	0.00030	4.719	4.65	64.475	1.864	447.7
2000.00	.03	792	3436.3	11.616	1.3116	0.7041	269	0.00025	5.02	4.704	107.316	1.904	457.5
4000.00	.02	670	3349.8	11.616	1.3234	0.7001	226	0.00021	5.730	4.76	178.419	1.938	465.6
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	60.00	3128	5138.3	12.360	1.1266	3.1609	811	0.00273	0.000	2.12	1.12	0.000	0.0
1.05	57.14	3114	5113.8	12.375	1.1268	3.1556	809	0.00270	0.295	3.17	2.12	1.198	46.1
1.20	50.00	3078	5047.5	12.417	1.1268	3.0546	801	0.00262	0.574	3.01	1.240	3.81	86.9
1.40	42.86	3037	4972.3	12.446	1.1264	2.9793	798	0.00254	0.780	2.95	1.051	5.15	120.2
1.50	37.50	3001	4908.1	12.450	1.1265	2.9028	793	0.00246	0.966	2.88	1.005	6.07	141.5
1.73	34.75	2981	4871.9	12.457	1.1260	2.8581	790	0.00241	1.000	2.87	1.000	6.52	152.2
2.00	30.00	2943	4803.0	12.470	1.1268	2.7698	784	0.00233	1.151	2.89	1.045	.732	170.8
4.00	15.00	2761	4492.8	12.4762	1.1301	2.5662	756	0.00191	1.630	3.15	1.353	1.016	237.0
4.08	14.70	2756	4494.0	12.4767	1.1303	2.5126	757	0.00190	1.643	3.16	1.369	1.022	238.6
10.00	6.00	2517	4119.3	12.4975	1.1422	1.7290	719	0.00138	2.151	3.54	2.414	1.276	297.8
20.00	3.00	2320	3883.7	13.094	1.1599	1.6390	685	0.00105	2.498	3.79	3.943	1.427	333.0
40.00	1.50	2108	3631.4	13.168	1.1647	1.0559	644	0.00080	2.828	4.003	6.551	1.552	362.1
100.00	.60	1813	3360.7	13.208	1.2172	0.8583	579	0.00061	3.272	4.25	12.932	1.685	393.3
200.00	.30	1596	3183.1	13.215	1.2346	0.7942	525	0.00052	3.633	3.74	21.699	1.768	412.5
400.00	.15	1599	3027.4	13.216	1.2487	0.7553	470	0.00044	4.015	4.44	36.494	1.837	426.6
1000.00	.08	1156	2854.1	13.218	1.2670	0.7136	397	0.00036	4.557	4.65	72.060	1.911	446.0
2000.00	.03	996	2740.1	13.216	1.2814	0.6644	344	0.00030	5.000	4.711	122.269	1.928	456.8
4000.00	.02	893	2643.9	13.216	1.2922	0.6796	294	0.00029	5.481	4.77	205.294	1.998	465.9
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	60.00	3188	4586.9	13.470	1.1207	3.6135	835	0.00317	0.000	2.117	.197	44.6	0.0
1.05	57.14	3175	4564.0	13.488	1.1205	3.6578	833	0.00315	0.296	500.7	2.117	1.198	46.1
1.20	50.00	3141	4502.0	13.536	1.1199	3.5527	828	0.00309	0.573	314.4	1.238	3.80	86.0
1.40	42.86	3103	4451.5	13.593	1.1193	3.4973	823	0.00303	0.782	286.0	1.050	.514	118.3
1.60	37.50	3070	4371.3	13.641	1.1186	3.4461	818	0.00297	0.928	279.0	1.005	.606	137.0
1.72	34.65	3052	4358.7	13.667	1.1186	3.4169	813	0.00293	1.000	278.3	1.000	.650	147.0
2.00	30.00	3016	4274.7	13.721	1.1181	3.3544	810	0.00286	1.134	280.3	1.016	.731	162.3
4.00	15.00	2893	3980.7	13.961	1.1170	3.0181	765	0.00291	1.655	306.6	1.361	1.015	229.7
4.08	14.70	2888	3972.4	13.968	1.1170	3.0070	762	0.00290	1.648	307.5	1.376	1.022	231.2
10.00	6.00	2665	3625.9	14.254	1.1504	2.4611	754	0.00199	2.158	3.44	2.455	1.278	289.2
20.00	3.00	2467	3379.6	14.490	1.1292	1.9810	727	0.00177	2.505	3.70	4.050	1.433	324.1
40.00	1.50	2321	3151.6	14.611	1.1306	1.0584	694	0.00117	2.826	3.924	6.873	1.552	355.4
100.00	.60	2074	2878.0	14.750	1.1703	1.0340	649	0.00078	3.252	4.17	13.944	1.704	382.5
200.00	.30	1868	2695.0	14.797	1.1892	0.8417	604	0.00061	3.548	4.32	23.785	1.739	405.7
400.00	.15	1658	2531.0	14.812	1.2191	0.7527	552	0.00051	3.894	4.45	40.475	1.870	422.9
1000.00	.06	1398	2343.4	14.816	1.2303	0.6975	479	0.00041	4.395	4.60	81.660	1.953	441.8
2000.00	.03	1220	2221.8	14.816	1.2515	0.6676	424	0.00035	4.806	4.69	138.794	2.006	453.6
4000.00	.02	1038	2116.0	14.816	1.2674	0.6395	370	0.00030	5.425	4.77	235.555	2.020	463.7
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	60.00	3213	4142.9	14.479	1.1182	3.7568	852	0.00335	0.000	2.117	.197	43.2	0.0
1.05	57.14	3201	4121.5	14.499	1.1179	3.7501	850	0.00333	0.296	484.9	2.117	1.198	43.2
1.20	50.00	3188	4065.3	14.553	1.1174	3.7255	849	0.00329	0.574	307.5	1.238	.500	53.2
1.40	42.86	3121	3997.2	14.616	1.1163	3.6542	840	0.00325	0.783	277.1	1.050	.514	112.6
1.60	37.50	3099	3940.7	14.669	1.1157	3.6672	833	0.00320	0.929	270.3	1.005	.605	132.7
1.72	34.65	3082	3910.6	14.698	1.1153	3.6048	833	0.00318	1.000	267.7	1.000	.644	142.2
2.00	30.00	3047	3648.1	14.759	1.1146	3.5123	828	0.00313	1.139	271.6	1.017	.731	160.2
4.00	15.00	2892	3573.5	15.031	1.1118	3.4121	804	0.00288	1.637	297.3	1.364	1.015	222.6
4.08	14.70	2888	3565.7	15.039	1.1117	3.4029	804	0.00287	1.655	298.2	1.379	1.022	224.1
10.00	6.00	2701	3238.7	15.377	1.1995	3.0640	774	0.00250	2.161	3.34	2.670	1.279	280.5
20.00	3.00	2564	3004.8	15.623	1.1043	2.7328	752	0.00217	2.509	3.59	4.112	1.422	314.7
40.00	1.50	2429	2788.4	15.856	1.1115	2.3591	728	0.00182	2.832	3.821	7.032	1.557	343.6
100.00	.60	2466	2520.2	16.124	1.1212	1.6259	692	0.00131	3.254	4.07	14.621	1.714	375.0
200.00	.30	2079	2335.5	16.278	1.1403	1.2476	694	0.00093	3.521	4.24	25.591	1.857	396.6
400.00	.15	1919	2166.1	16.370	1.1721	0.8700	629	0.00060					

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID (XYGEN)

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb./sq.in abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscos-ity, μ, micro poises	Thermal conductivity, k, cal/(sec·°K/cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb-sec/lb)	Area ratio, ε	Thrust coefficient, C _t	Specific impulse, I, (lb-sec/lb)
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	60.00	3217	3777.9	15.399	1.1174	3.6327	864	0.01328	0.000	2.115	0.000	0.000	0.0
1.05	57.14	3205	3757.7	15.420	1.1171	3.6262	862	0.01327	2.296	470.6	0.197	41.9	
1.20	50.00	3175	3702.9	15.478	1.1163	3.6075	858	0.01323	574	300.2	1.237	3.80	80.8
1.40	42.86	3136	3640.5	15.545	1.1154	3.5839	852	0.01319	784	268.9	1.050	514	109.3
1.60	37.50	3104	3587.4	15.602	1.1147	3.5616	847	0.01315	830	264.4	1.005	605	128.7
1.72	34.91	3084	3559.2	15.633	1.1141	3.5493	845	0.01313	1.000	261.7	1.000	648	137.9
2.00	30.00	3053	3500.2	15.698	1.1136	3.5214	840	0.01309	1.136	263.6	1.017	730	155.4
4.00	15.00	2900	3241.5	15.990	1.1104	3.3685	816	0.01288	1.637	284.6	1.364	1.015	216.0
4.08	14.70	2896	3234.1	15.998	1.1103	3.3631	816	0.01287	1.650	289.5	1.380	1.022	217.5
10.00	6.00	2713	2925.7	16.363	1.1047	3.1047	786	0.01256	2.161	324.9	2.474	1.280	272.3
20.00	3.00	2579	2704.9	16.634	1.1060	2.8627	784	0.01230	2.509	349.4	4.124	1.436	305.6
40.00	1.50	2452	2498.2	16.894	1.1077	2.5882	742	0.01203	2.833	371.3	7.068	1.568	333.7
100.00	.60	2287	2245.4	17.213	1.1075	2.1075	711	0.01166	3.237	396.6	14.785	1.716	365.2
200.00	.30	2164	2088.3	17.431	1.1113	1.6812	687	0.01138	3.532	415.5	26.152	1.813	385.7
400.00	.15	2037	1903.2	17.624	1.1181	1.5563	660	0.01111	3.820	428.6	46.510	1.898	403.9
1000.00	.08	1859	1705.0	17.620	1.1190	1.1940	619	0.00979	4.197	446.1	99.697	1.997	424.9
2000.00	.03	1710	1565.5	17.928	1.1194	.8974	581	0.00980	4.487	457.6	176.636	2.052	438.8
4000.00	.02	1549	1440.4	17.985	1.1089	.731d	537	0.00947	4.798	467.5	310.311	2.119	451.0
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	60.00	3116	2626.1	18.987	1.1200	2.2973	889	0.00216	0.000	2.117	0.000	0.000	0.0
1.05	57.14	3103	2610.4	19.010	1.1198	2.2869	887	0.00214	2.295	417.0	2.117	3.72	
1.20	50.00	3070	2567.2	19.074	1.1193	2.2574	884	0.00210	574	266.0	1.238	3.80	71.6
1.40	42.86	3031	2518.3	19.147	1.1181	2.2216	875	0.00200	.783	238.2	1.050	514	96.8
1.60	37.50	2999	2476.8	19.210	1.1185	2.1692	869	0.00192	.928	232.4	1.005	605	114.1
1.72	34.91	2901	2424.0	19.244	1.1181	2.1710	867	0.00194	1.000	231.8	1.000	650	122.4
2.00	30.00	2949	2408.2	19.313	1.1171	2.1523	861	0.00195	1.134	233.4	1.016	731	137.7
4.00	15.00	2762	2409.0	19.623	1.1107	1.9393	633	0.00172	1.639	255.4	1.361	1.015	191.3
4.08	14.70	2777	2199.9	19.632	1.1107	1.9277	632	0.00171	1.648	256.1	1.377	1.022	192.6
10.00	6.00	2576	1959.5	19.999	1.1163	1.6500	796	0.01140	2.158	287.1	2.454	1.278	240.8
20.00	3.00	2421	1766.5	20.250	1.1242	1.3799	767	0.01119	2.508	308.3	4.065	1.433	270.0
40.00	1.50	2263	1630.0	20.463	1.1311	1.2482	736	0.01092	2.810	326.9	6.896	1.563	294.4
100.00	.60	2040	1439.4	20.667	1.1538	.8544	686	0.00966	3.238	347.9	14.098	1.706	321.3
200.00	.30	1856	1309.4	20.755	1.1748	.6739	645	0.00921	3.545	361.3	24.259	1.796	338.4
400.00	.15	1604	1193.0	20.795	1.2033	.5774	595	0.00931	3.870	372.7	41.606	1.874	353.1
1000.00	.08	1415	1028.4	20.810	1.2202	.5120	524	0.00933	4.547	385.2	84.484	1.961	369.3
2000.00	.03	1240	970.8	20.812	1.2443	.4470	465	0.00929	4.745	395.1	144.082	2.015	379.5
4000.00	.02	1000	955.9	20.813	1.2596	.4070	416	0.00924	5.173	399.6	245.360	2.061	388.2
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	60.00	2966	2016.0	12.453	1.1264	1.5209	886	0.00145	0.000	2.122	0.000	0.000	0.0
1.05	57.14	2953	2002.7	12.476	1.1263	1.5098	884	0.00144	.295	382.7	2.122	.198	34.1
1.20	50.00	2917	1966.4	12.537	1.1264	1.4788	878	0.00140	.572	244.0	1.240	.381	65.7
1.40	42.86	2877	1925.3	12.606	1.1265	1.4419	870	0.00135	.780	218.4	1.052	.515	88.8
1.60	37.50	2811	1890.2	12.665	1.1267	1.4091	864	0.00132	.926	213.0	1.005	.607	104.6
1.72	34.91	2821	1870.4	12.678	1.1268	1.3901	861	0.00129	1.000	212.4	1.000	.653	112.6
2.00	30.00	2783	1834.8	12.761	1.1272	1.3229	854	0.00125	1.131	213.8	1.015	.732	126.3
4.00	12.00	2604	1663.4	12.932	1.1309	1.1600	821	0.00105	1.630	233.5	1.353	1.016	175.2
4.08	14.70	2599	1628.6	12.943	1.1310	1.1632	820	0.00102	1.642	234.2	1.366	1.022	176.4
10.00	6.00	2365	1454.5	12.933	1.1424	.9620	774	0.00080	2.152	261.7	2.412	1.276	220.1
20.00	3.00	2177	1319.4	12.946	1.1502	.7201	731	0.00063	2.500	280.1	3.941	1.427	246.1
40.00	1.50	1976	1292.4	12.960	1.1608	.6166	689	0.00050	2.831	295.9	6.557	1.552	267.6
100.00	.60	1706	1044.7	22.660	1.2122	.5100	621	0.00038	3.273	313.1	12.980	1.685	290.7
200.00	.30	1503	947.4	22.673	1.2308	.4699	566	0.00033	3.629	323.8	21.822	1.768	305.0
400.00	.15	1310	861.6	22.677	1.2470	.4457	510	0.00028	4.008	332.8	36.754	1.888	316.9
1000.00	.08	1095	764.9	22.677	1.2560	.4221	438	0.0023	4.546	342.6	73.335	1.913	329.9
2000.00	.03	945	703.1	22.677	1.2749	.4064	386	0.00240	4.986	348.7	123.637	1.960	338.0
4000.00	.02	821	649.8	22.677	1.2562	.3916	337	0.00117	5.460	359.8	208.163	1.999	344.8
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	60.00	2625	1381.4	24.532	1.1502	0.8140	521	0.00178	0.000	2.140	0.000	0.000	0.0
1.05	57.14	2640	1370.9	24.548	1.1510	0.808	548	0.00177	.292	530.6	2.140	.199	30.2
1.20	50.00	2599	13427	24.521	1.1529	.7759	500	0.00174	.566	215.4	1.248	.384	58.1
1.40	42.86	2520	1310.6	24.603	1.1524	.7506	531	0.00171	.772	192.5	1.026	.519	78.5
1.60	37.50	2509	1283.4	24.676	1.1529	.7260	522	0.00168	.915	187.5	1.007	.611	92.3
1.72	34.91	2481	1265.7	24.700	1.1526	.7099	516	0.00166	1.000	186.9	1.000	.664	100.3
2.00	30.00	2438	1239.0	24.735	1.1624	.6892	498	0.00163	1.118	187.9	1.013	.736	111.3
4.00	15.00	2216	1109.8	24.876	1.1809	.5739	760	0.00151	1.612	203.8	1.325	1.017	153.7
4.08	14.70	2209	1106.2	24.879	1.1815	.5710	759	0.00151	1.625	206.4	1.339	1.023	154.8
10.00	6.00	1915	958.4	24.972	1.2107	.4712	690	0.00139	2.140	226.3	2.286	1.268	191.7
20.00	3.00	1691	859.6	24.998	1.2309	.4277	635	0.00133	2.512	240.5	3.629	1.409	213.1
40.00	1.50	1480	772.3	25.006	1.2463	.4030	575	0.00129	2.883	252.4	5.877	1.522	230.2
100.00	.60	1249	673.9	25.008	1.2627	.3820	500	0.00124	3.586	265.2	11.319	1.641	248.1
200.00	.30	1061	611.0	25.008	1.2749	.3600	446	0.00121	.787	275.1	18.732	1.712	258.9
400.00	.15	911	556.7	25.008	1.2872	.3561	399	0.00118	4.207	279.6	31.103	1.771	

TABLE III. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P lb/sq.in. abs	Static pressure, P_c lb/sq.in. abs	Temper- ature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/(deg*K)*	Viscos- ity, μ , micro poises	Thermal conductivity, k , cal/(sec*°K*cm)	Mach number M	Specific impulse in vacuum, I_{vac} , (lb/Sec)/lb	Area ratio, ϵ	Thrust coefficient, impulse: C_F , lb/(sec/lb)	
$R = 4.000$, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	60.00	2347	1054.4	26.257	1.1871	0.2285	798	0.00050	0.000	0.000	0.000	0.0	
1.05	57.14	2350	1049.8	26.265	1.1885	0.227	795	0.00049	2.165	0.202	27.4		
1.20	50.00	2282	1022.5	26.260	1.1745	0.2073	784	0.00047	1.260	0.388	52.7		
1.40	42.86	2228	996.2	26.307	1.1972	0.4906	772	0.00043	1.051	0.524	71.2		
1.60	37.50	2180	974.0	26.323	1.2013	0.4772	761	0.00042	1.009	0.616	83.6		
1.78	35.79	2143	957.0	26.334	1.2046	0.4674	753	0.00042	1.000	0.678	92.1		
2.00	30.00	2101	937.9	26.345	1.2084	0.4589	743	0.00041	1.010	0.742	100.7		
4.00	15.00	1856	834.6	26.367	1.2292	0.4102	682	0.00035	1.297	1.019	138.3		
4.08	14.70	1851	831.7	26.388	1.2298	0.4092	683	0.00034	1.311	1.026	139.2		
10.00	6.00	1556	217.0	26.403	1.2303	0.3769	606	0.00029	2.165	2.192	171.3		
20.00	3.00	1351	641.3	26.406	1.2347	0.3619	547	0.00025	2.129	3.439	1.397	189.6	
40.00	1.50	1167	575.7	26.408	1.2358	0.3501	491	0.00022	2.128	5.518	1.504	204.1	
100.00	.60	954	502.6	26.406	1.2393	0.3354	422	0.00018	3.452	4.333	10.507	219.1	
200.00	.30	815	456.7	26.406	1.2392	0.3244	372	0.00016	3.870	2.397	17.236	1.681	228.0
400.00	.15	692	417.5	26.406	1.2312	0.3141	326	0.00013	4.314	2.450	26.358	1.735	235.4
1000.00	.06	553	374.8	26.406	1.2349	0.3013	270	0.00011	4.951	2.506	54.842	1.792	243.2
2000.00	.03	464	349.3	26.406	1.2348	0.2929	236	0.00009	5.484	2.540	90.278	1.827	247.9
4000.00	.02	387	326.2	26.406	1.2363	0.2865	197	0.00008	6.070	2.568	148.471	1.855	251.7
$R = 5.000$, PERCENT FUEL = 24.458, O/F = 39.683													
1.00	60.00	2062	855.0	27.299	1.2228	0.4109	740	0.00037	0.000	0.000	0.000	0.0	
1.05	57.14	2044	847.7	27.302	1.2242	0.4079	736	0.00037	2.186	0.204	25.2		
1.20	50.00	1995	828.1	27.309	1.2290	0.4004	724	0.00036	1.269	0.392	48.4		
1.40	42.86	1938	809.0	27.316	1.2323	0.3925	710	0.00034	1.066	0.529	65.3		
1.60	37.50	1890	787.4	27.321	1.2338	0.3864	698	0.00033	0.92	1.011	62.1		
1.80	33.40	1849	771.7	27.324	1.2347	0.3816	688	0.00033	1.000	0.690	85.1		
2.00	30.00	1811	757.4	27.327	1.2414	0.3775	679	0.00032	1.093	1.007	747	92.2	
4.00	17.00	1576	674.1	27.336	1.2590	0.3519	617	0.00026	1.294	1.022	126.2		
4.08	14.70	1571	669.7	27.336	1.2590	0.3519	617	0.00026	1.297	1.029	127.0		
10.00	6.00	1304	576.3	27.338	1.2707	0.3413	559	0.00023	2.151	2.184	2.161	155.7	
20.00	3.00	1122	515.3	27.339	1.2815	0.3209	484	0.00020	2.049	1.926	3.345	1.393	171.9
40.00	1.50	961	462.9	27.339	1.2928	0.3009	432	0.00018	2.046	5.334	1.490	184.7	
100.00	.60	778	405.1	27.339	1.3094	0.3076	367	0.00015	3.486	2.103	10.072	1.603	197.8
200.00	.30	659	369.0	27.339	1.3227	0.2979	321	0.00012	3.918	2.158	16.410	1.666	205.6
400.00	.15	555	338.5	27.339	1.3364	0.2888	279	0.00011	4.379	2.203	26.810	1.717	212.0
1000.00	.06	438	305.6	27.339	1.3536	0.2763	230	0.00008	5.047	2.250	51.370	1.771	218.6
2000.00	.03	365	285.4	27.339	1.3632	0.2728	195	0.00007	5.611	2.278	84.049	1.804	224.6
4000.00	.02	303	268.6	27.339	1.3697	0.2693	164	0.00006	6.254	2.301	137.526	1.830	225.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P ₀	Static pressure, P, lb/in. ²	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec·°K)/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , lb-sec/lb	Area ratio, ε	Thrust coefficient, C _F	Specific impulse, I, lb-sec/lb
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	150.00	1183	5313.5	4.416	1.3396	1.7752	.314	0.00073	1.000			0.000	0.0
1.05	142.86	1168	5287.7	4.416	1.3406	1.7711	.311	0.00073	.271	530.0	2.250	.210	47.4
1.20	125.00	1129	5218.7	4.416	1.3436	1.7597	.303	0.00070	.527	334.2	1.297	.403	90.8
1.40	107.14	1085	5141.8	4.416	1.3469	1.7473	.294	0.00068	.722	296.1	1.081	.543	122.2
1.60	93.75	1049	5077.7	4.416	1.3497	1.7368	.285	0.00066	.880	286.6	1.018	.636	145.2
1.87	80.42	1008	5006.8	4.416	1.3527	1.7257	.276	0.00063	1.000	284.1	1.000	.725	165.4
2.00	75.00	989	4975.4	4.416	1.3541	1.7210	.272	0.00062	1.059	284.4	1.003	.761	171.5
4.00	37.50	824	4693.4	4.416	1.3651	1.6882	.234	0.00052	1.566	301.7	1.233	1.031	232.3
10.00	15.00	643	4392.5	4.416	1.3748	1.6505	.186	0.00042	2.152	327.5	1.974	1.257	283.1
10.21	14.70	639	4388.6	4.416	1.3750	1.6591	.187	0.00041	2.165	328.1	1.997	1.261	284.0
20.00	7.50	532	4259.0	4.416	1.3800	1.6343	.159	0.00035	2.286	343.5	2.982	1.376	309.9
4.00	3.75	439	4058.9	4.416	1.3822	1.6269	.133	0.00029	3.031	356.4	4.620	1.467	330.4
100.00	1.50	340	3849.0	4.416	1.3882	1.6091	.104	0.00023	3.484	369.8	8.432	1.558	350.8
200.00	.75	280	3802.6	4.416	1.3923	1.5771	.085	0.00018	4.149	377.7	13.431	1.610	362.6
400.00	.38	230	3723.2	4.416	1.4070	1.5596	.070	0.00015	4.674	384.1	21.488	1.652	372.0
1000.00	.15	175	3640.1	4.416	1.4350	1.4845	.055	0.00011	5.438	390.6	39.928	1.694	381.6
2000.00	.08	142	3590.9	4.416	1.4552	1.4387	.045	0.00009	6.096	394.3	63.572	1.719	387.2
4000.00	.04	114	3551.2	4.416	1.4710	1.4054	.036	0.00007	6.844	397.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	150.00	1514	2969.7	5.216	1.3078	1.6191	.402	0.00084	1.000			0.000	0.0
1.05	142.86	1497	2941.7	5.216	1.3089	1.6146	.399	0.00083	.274	552.1	2.233	.207	49.3
1.20	145.00	1450	2866.8	5.216	1.3119	1.6062	.389	0.00081	.533	348.6	1.289	.400	94.6
1.40	107.14	1398	2783.1	5.216	1.3124	1.5889	.378	0.00078	.730	309.3	1.077	.539	127.4
1.60	93.75	1354	2713.2	5.216	1.3185	1.5773	.369	0.00076	.869	299.6	1.016	.632	149.4
1.85	81.25	1307	2660.5	5.216	1.3217	1.5652	.359	0.00073	1.000	297.3	1.000	.716	169.2
2.00	75.00	1282	2601.1	5.216	1.3256	1.5585	.353	0.00072	1.068	297.8	1.004	.757	179.1
4.00	37.50	1079	2290.0	5.216	1.3391	1.5045	.307	0.00061	1.572	316.7	1.244	1.029	243.2
10.00	15.00	852	1954.3	5.216	1.3558	1.4516	.251	0.00048	2.148	344.7	2.009	1.257	297.2
10.21	14.70	847	1947.7	5.216	1.3562	1.4506	.250	0.00048	2.161	345.3	2.033	1.261	298.2
20.00	7.50	709	1748.8	5.216	1.3655	1.4232	.213	0.00040	2.473	362.0	3.049	1.379	325.9
4.00	3.75	588	1578.0	5.216	1.3714	1.4067	.179	0.00034	3.010	376.0	4.739	1.472	348.0
100.00	1.50	458	1396.3	5.216	1.3770	1.3914	.142	0.00026	5.619	390.5	8.679	1.555	370.0
200.00	.75	379	1286.1	5.216	1.3811	1.3807	.117	0.00024	6.111	399.1	13.670	1.619	382.7
400.00	.38	312	1195.2	5.216	1.3861	1.3875	.096	0.00018	6.638	406.1	22.495	1.662	393.0
1000.00	.15	242	1098.9	5.216	1.3972	1.3402	.074	0.00013	7.394	413.4	41.779	1.700	405.5
2000.00	.08	198	1041.1	5.216	1.4164	1.2958	.061	0.00011	8.012	417.7	67.687	1.735	409.7
4000.00	.04	161	993.9	5.216	1.4344	1.2580	.050	0.00009	8.708	421.1	109.754	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	150.00	1816	1249.3	6.016	1.2820	1.5040	.481	0.00092	1.000			0.000	0.0
1.05	142.86	1797	1220.2	6.016	1.2831	1.4992	.477	0.00091	.277	563.4	2.218	.207	50.3
1.20	125.00	1745	1124.1	6.016	1.2880	1.4867	.467	0.00089	.538	356.2	1.283	.398	96.6
1.40	107.14	1686	1054.7	6.016	1.2893	1.4730	.459	0.00086	.736	316.3	1.073	.556	130.1
1.60	93.75	1626	981.2	6.016	1.2921	1.4616	.446	0.00084	.876	304.6	1.015	.629	152.7
1.83	81.40	1587	910.0	6.016	1.2950	1.4503	.430	0.00081	1.000	304.5	1.000	.708	171.8
2.00	75.00	1555	863.9	6.016	1.2970	1.4449	.429	0.00080	1.076	305.1	1.005	.754	183.1
4.00	37.50	1322	555.1	6.016	1.3125	1.3875	.376	0.00068	1.578	325.5	1.256	1.027	249.3
10.00	15.00	1057	178.1	6.016	1.3329	1.3225	.314	0.00046	2.147	355.1	2.048	1.258	305.6
10.21	14.70	1052	169.0	6.016	1.3333	1.3213	.314	0.00046	2.159	355.4	2.073	1.262	306.6
20.00	7.50	887	959.0	6.016	1.3461	1.2847	.269	0.00046	2.563	373.7	3.127	1.384	335.7
4.00	3.75	741	976.0	6.016	1.3585	1.2559	.220	0.00038	2.987	388.7	4.683	1.478	359.0
100.00	1.50	581	9569.1	6.016	1.3663	1.2320	.181	0.00030	3.581	404.2	8.985	1.574	382.4
200.00	.75	462	9447.8	6.016	1.3717	1.2190	.151	0.00029	4.064	413.4	14.396	1.630	395.9
400.00	.38	399	9367.3	6.016	1.3755	1.2100	.125	0.00020	4.384	420.9	23.208	1.675	406.8
1000.00	.15	310	9240.5	6.016	1.3817	1.1923	.095	0.00017	5.327	426.7	45.894	1.722	416.1
2000.00	.08	229	9173.9	6.016	1.3860	1.1803	.078	0.00014	5.949	435.4	71.600	1.749	424.7
4000.00	.04	210	9122.7	6.016	1.4039	1.1601	.064	0.00010	6.606	437.2	115.621	1.771	430.2
R = 0.300, PERCENT FUEL = 29.67, O/F = 2.381													
1.00	150.00	204	9932.7	6.813	1.2583	1.4448	.550	0.00099	1.000			0.000	0.0
1.05	142.86	2071	9903.1	6.814	1.2592	1.4282	.547	0.00098	.279	560.4	2.405	.206	50.8
1.20	125.00	2015	9824.6	6.814	1.2627	1.4111	.537	0.00097	.542	359.7	1.217	.375	97.5
1.40	107.14	1951	9734.4	6.815	1.2653	1.3931	.525	0.00092	.742	319.8	1.070	.553	131.4
1.60	93.75	1897	9659.5	6.815	1.2694	1.3786	.515	0.00090	.882	310.3	1.013	.626	148.2
1.83	82.65	1846	9590.3	6.815	1.2723	1.3659	.505	0.00087	1.000	308.4	1.000	.700	172.6
2.00	75.00	1807	9539.0	6.816	1.2744	1.3567	.496	0.00086	1.082	309.4	1.006	.751	185.1
4.00	37.50	1553	9199.0	6.816	1.2899	1.2995	.445	0.00074	1.585	330.5	1.266	1.029	242.5
10.00	15.00	1220	8825.4	6.816	1.3070	1.2557	.375	0.00060	2.140	361.8	2.085	1.259	310.4
10.21	14.70	1251	8817.9	6.816	1.3099	1.2524	.374	0.00060	2.160	362.4	2.111	1.264	311.5
20.00	7.50	1064	8591.3	6.816	1.3240	1.1891	.325	0.00051	2.525	381.4	3.006	1.386	341.7
4.00	3.75	893	8533.7	6.816	1.3304	1.1531	.279	0.00044	2.960	397.0	5.037	1.400	366.0
100.00	1.50	708	8140.4	6.816	1.3530	1.1170	.225	0.00033	3.544	413.0	9.025	1.584	370.5
200.00	.75	590	8049.7	6.816	1.3502	1.1008	.187	0.00027	4.013	425.3	14.994	1.664	404.8
400.00	.38	490	7940.9	6.816	1.3566	1.0868	.150	0.00023	4.517	431.4	24.235	1.689	416.3
1000.0													

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P_s , lb/in ² abs	Temperature, T_s , °K	Enthalpy, h_s , cal/g	Molecular weight, \overline{M}	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec·°K)·cm	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb/sec)/lb	Area ratio, ϵ	Thrust coefficient, C_T	Specific impulse, I , lb·sec/lb
$R = 0.350$, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	150.00	2339	8892.8	7.604	1.2338	1.4271	610	0.00107	0.000	569.2	2.192	0.000	0.0
1.05	142.86	2317	8862.1	7.605	1.2352	1.4164	606	0.00106	.282	360.7	1.271	.393	50.8
1.20	125.00	2259	8783.3	7.607	1.2391	1.3889	597	0.00102	.547	321.0	1.067	.530	97.6
1.40	107.14	2193	8692.6	7.609	1.2454	1.3804	585	0.00099	.748	311.6	1.012	.623	154.6
1.60	93.75	2137	8616.1	7.611	1.2471	1.3585	576	0.00096	.889	309.8	1.000	.693	172.1
1.80	83.19	2087	8552.2	7.612	1.2502	1.3209	567	0.00093	1.000	304.7	1.007	.748	185.7
2.00	75.00	2044	8496.3	7.613	1.2528	1.3068	559	0.00091	1.089	310.7	1.007	.748	185.7
4.00	37.50	1772	8151.6	7.615	1.2690	1.2337	506	0.00079	1.590	333.1	1.276	1.023	254.0
10.00	15.00	1451	7767.3	7.616	1.2886	1.1659	434	0.00065	2.148	365.6	2.120	1.260	312.9
10.21	14.70	1444	7759.5	7.616	1.2888	1.1645	433	0.00065	2.160	366.2	2.147	1.265	314.0
20.00	7.50	1239	7524.4	7.616	1.3035	1.1206	381	0.00055	2.549	385.8	3.282	1.390	345.1
40.00	3.75	1051	7317.8	7.616	1.3188	1.0794	330	0.00046	2.952	402.4	5.191	1.491	370.2
100.00	1.50	838	7012.8	7.616	1.3364	1.0366	267	0.00036	3.510	419.8	9.681	1.594	395.8
200.00	.75	702	6953.8	7.616	1.3475	1.0119	226	0.00030	3.963	430.2	15.634	1.654	410.8
400.00	.38	586	6837.5	7.616	1.3553	.9953	189	0.00025	4.452	438.6	25.362	1.703	422.9
1000.00	.15	460	6713.0	7.616	1.3636	.9789	148	0.00019	5.160	447.5	48.312	1.754	435.5
2000.00	.08	342	6627.0	7.616	1.3663	.9694	121	0.00016	5.750	452.8	78.890	1.784	443.0
4000.00	.04	317	6574.0	7.616	1.3739	.9587	98	0.00013	6.390	457.2	129.010	1.809	449.2
$R = 0.400$, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	150.00	2553	8050.5	8.379	1.2094	1.4879	660	0.00118	0.000	566.8	2.178	0.000	0.0
1.05	142.86	2532	8021.1	8.382	1.2108	1.4725	657	0.00116	.284	359.6	1.265	.391	50.6
1.20	125.00	2475	7949.1	8.388	1.2148	1.4323	648	0.00112	.552	320.4	1.064	.527	131.2
1.40	107.14	2410	7852.7	8.393	1.2194	1.3894	637	0.00107	.754	320.4	1.064	.527	131.2
1.60	93.75	2359	7777.5	8.398	1.2235	1.3555	628	0.00104	.895	311.3	1.011	.619	156.1
1.79	83.64	2306	7715.9	8.401	1.2269	1.3293	620	0.00101	1.000	309.7	1.000	.686	170.6
2.00	75.00	2260	7655.7	8.404	1.2302	1.3052	612	0.00098	1.096	310.8	1.008	.745	185.3
4.00	37.50	1978	7308.9	8.413	1.2491	1.1954	561	0.00084	1.594	334.1	1.286	1.021	254.0
10.00	15.00	1638	6918.4	8.416	1.2695	1.1133	489	0.00069	2.147	367.5	2.155	1.261	313.9
10.21	14.70	1631	6910.5	8.416	1.2699	1.1119	488	0.00069	2.159	366.2	2.182	1.266	315.0
20.00	7.50	1410	6669.3	8.416	1.2841	1.0674	435	0.00059	2.542	388.5	3.350	1.393	346.7
40.00	3.75	1206	6455.6	8.416	1.2991	1.0256	380	0.00050	2.937	405.8	5.344	1.497	372.5
100.00	1.50	971	6220.8	8.416	1.3187	.9769	313	0.00040	3.479	424.0	10.047	1.604	399.0
200.00	.75	819	6074.6	8.416	1.3317	.9479	266	0.00033	3.917	434.9	16.311	1.666	414.6
400.00	.38	688	5951.6	8.416	1.3427	.9251	224	0.00027	4.388	443.9	26.573	1.717	427.4
1000.00	.15	543	5819.0	8.416	1.3535	.9090	176	0.00021	5.072	453.3	50.851	1.771	440.6
2000.00	.08	452	5737.8	8.416	1.3595	.8930	146	0.00019	5.644	458.9	83.233	1.803	448.6
4000.00	.04	376	5670.2	8.416	1.3649	.8832	119	0.00014	6.266	463.6	136.502	1.829	455.1
$R = 0.450$, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	150.00	2733	7354.5	9.133	1.1879	1.6077	701	0.00132	0.000	562.0	2.165	0.000	0.0
1.05	142.86	2713	7325.6	9.137	1.1891	1.5851	698	0.00130	.287	562.0	2.165	.202	50.6
1.20	125.00	2659	7247.6	9.148	1.1925	1.5361	690	0.00125	.557	357.0	1.259	.388	96.4
1.40	107.14	2596	7159.7	9.159	1.1966	1.4792	681	0.00119	.760	318.4	1.061	.524	130.2
1.60	93.75	2542	7085.3	9.168	1.2004	1.4330	672	0.00115	.902	309.6	1.009	.616	153.0
1.77	84.52	2499	7028.7	9.174	1.2034	1.3991	666	0.00111	1.000	308.3	1.000	.678	168.4
2.00	75.00	2451	6964.7	9.181	1.2070	1.3621	658	0.00107	1.103	309.5	1.009	.742	184.2
4.00	37.50	2171	6610.6	9.192	1.2262	1.1951	610	0.00089	1.599	333.6	1.298	1.019	253.0
10.00	15.00	1819	6224.7	9.215	1.2519	1.0768	541	0.00073	2.145	368.0	2.193	1.263	313.5
10.21	14.70	1812	6216.7	9.215	1.2523	1.0750	539	0.00072	2.156	368.7	2.221	1.267	314.7
20.00	7.50	1578	5971.1	9.216	1.2604	1.0228	486	0.00063	2.534	384.6	3.436	1.397	346.9
40.00	3.75	1359	5751.9	9.216	1.2808	.9435	430	0.00054	2.922	407.6	5.502	1.504	373.4
100.00	1.50	1106	5509.0	9.216	1.3306	.9330	359	0.00043	3.450	426.6	10.428	1.614	400.7
200.00	.75	939	5356.4	9.216	1.3310	.9001	308	0.00036	3.673	438.1	17.026	1.679	417.0
400.00	.38	794	5227.1	9.216	1.3320	.8730	262	0.00030	4.327	447.5	27.879	1.733	430.2
1000.00	.15	631	5086.9	9.216	1.3417	.8467	207	0.00023	4.986	457.5	53.635	1.789	444.2
2000.00	.08	528	5000.6	9.216	1.3501	.8316	174	0.00019	5.236	463.5	88.103	1.823	452.6
4000.00	.04	440	4928.4	9.216	1.3561	.8211	143	0.00016	6.139	468.4	144.834	1.851	459.5
$R = 0.500$, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	150.00	2881	6769.6	9.859	1.1704	1.7727	736	0.00149	0.000	555.6	2.153	.201	49.6
1.05	142.86	2862	6741.4	9.860	1.1713	1.7501	733	0.00147	.289	553.3	1.254	.386	95.3
1.20	125.00	2811	6650.4	9.863	1.1739	1.6693	726	0.00141	.561	353.3	1.254	.386	95.3
1.40	107.14	2752	6579.0	9.861	1.1771	1.6211	717	0.00134	.766	315.4	1.059	.522	128.8
1.60	93.75	2701	6506.0	9.863	1.1802	1.5642	710	0.00129	.908	307.0	1.008	.614	151.5
1.77	83.64	2664	6454.3	9.862	1.1825	1.5246	704	0.00125	1.000	305.7	1.000	.671	165.6
2.00	75.00	2615	6397.3	9.867	1.1856	1.4743	697	0.00120	1.110	307.1	1.011	.739	182.4
4.00	37.50	2346	6044.3	9.864	1.2061	1.2444	653	0.00098	1.605	332.1	1.311	1.018	251.2
10.00	15.00	1994	5649.4	10.010	1.2334	1.0852	587	0.00077	2.142	367.4	2.235	1.265	312.2
10.21	14.70	1986	5641.3	10.010	1.2339	1.0845	586	0.00077	2.154	368.1	2.264	1.270	313.3
20.00	7.50	1743	5392.6	10.010	1.2499	.9950	533	0.00066	2.524	389.6	3.522	1.403	346.1
40.00	3.75	1512	5169.1	10.010	1.2641	.9924	478	0.00057	2.905	408.2	5.670	1.512	373.2
100.00	1.50	1242	4919.2	10.010	1.2820	.9894	405	0.00046	3.421	428.0	10.829	1.626	401.3
200.00	.75	1053	4761.0	10.010	1.2900	.9842	351	0.00039	3.831	440.0	17.784	1.694	418.1
400.00	.38</td												

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OX₂/GEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P_s (lb/sq in abs)	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(lb)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(inch) ² (°K)(in)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/sec/lb	Area ratio, E	Thrust coefficient, C_T	Specific impulse, I , (lb/sec)/(lb)
$R = 0.600$; PERCENT FUEL = 17.35, O/F = 4.762													
1.00	150.00	3097	5841.6	11.228	1.1465	2.005	788	0.00191	0.000	5292	540.2	2.136	0.000
1.05	142.86	3081	5815.0	11.239	1.1489	2.1752	786	0.00188	0.292	540.2	1.247	1.199	48.2
1.20	125.00	3036	5742.8	11.268	1.1479	4.105	780	0.00181	0.267	544.0	1.055	1.383	92.7
1.40	107.14	2985	5661.1	11.300	1.1493	2.0248	773	0.00173	3.774	307.5	1.055	518	125.3
1.60	93.75	2940	5591.6	11.326	1.1507	1.9551	766	0.00167	9.18	299.6	1.007	610	147.5
1.74	86.09	2911	5547.9	11.343	1.1517	9.107	762	0.00162	1.000	298.7	1.000	.661	159.9
2.00	75.00	2865	5478.2	11.368	1.1535	1.8396	756	0.00155	1.122	300.4	1.013	.735	177.8
4.00	37.50	2630	5146.9	11.479	1.1602	1.5032	720	0.00121	1.618	326.4	1.333	1.017	245.9
10.00	15.00	2308	4756.8	11.570	1.1922	1.1596	666	0.00092	2.143	363.4	2.321	1.270	307.2
10.21	14.70	2300	4748.7	11.572	1.1928	1.1536	665	0.00091	2.154	364.1	2.352	1.275	308.4
20.00	7.50	2058	4497.3	11.602	1.2121	1.0010	619	0.00075	2.506	386.9	3.708	1.014	342.0
40.00	3.75	1815	4267.6	11.613	1.2327	.9136	566	0.00064	2.887	406.6	6.038	1.530	370.1
100.00	1.50	1518	4006.8	11.616	1.2517	.8515	493	0.00053	3.360	427.8	11.693	1.652	399.6
200.00	.75	1517	3838.9	11.616	1.2624	.8157	437	0.00045	3.749	440.9	19.413	1.726	417.4
400.00	.38	1155	3693.7	11.616	1.2798	.7825	383	0.00038	4.158	451.9	32.319	1.787	432.3
1000.00	.15	924	3592.7	11.616	1.2988	.7435	314	0.00030	4.742	463.6	63.444	1.853	448.2
2000.00	.08	766	3431.6	11.616	1.3122	.7189	267	0.00023	5.228	470.7	105.595	1.893	457.9
4000.00	.04	655	3345.7	11.616	1.3293	.6994	224	0.00020	5.759	476.6	175.548	1.927	466.0
$R = 0.700$; PERCENT FUEL = 15.25, O/F = 5.556													
1.00	150.00	3231	5138.3	12.482	1.1328	2.7036	825	0.00240	0.000	5294	523.5	2.126	0.000
1.05	142.86	3216	5113.3	12.497	1.1328	2.6809	823	0.00237	.294	523.5	1.242	.198	46.7
1.20	125.00	3176	5045.4	12.536	1.1328	2.6171	816	0.00230	.570	333.6	1.242	.382	89.8
1.40	107.14	3130	4968.6	12.580	1.1329	2.5409	811	0.00222	.778	298.5	1.052	.516	121.5
1.60	93.75	3091	4903.1	12.618	1.1331	2.4728	806	0.00215	.923	291.1	1.006	.607	143.1
1.73	86.09	3088	4865.0	12.640	1.1335	2.4518	803	0.0021	1.000	290.3	1.000	.655	154.2
2.00	75.00	3055	4759.5	12.680	1.1338	2.3350	797	0.00203	1.129	292.1	1.015	.733	172.6
4.00	37.50	2823	4480.4	12.855	1.1366	1.9694	767	0.0016	1.627	318.6	1.348	1.016	239.3
10.00	15.00	2550	4102.6	13.040	1.1534	1.4750	724	0.001.1	1.350	356.5	2.391	1.275	300.2
10.21	14.70	2544	4094.8	13.044	1.1539	1.4650	723	0.001.0	2.161	357.3	2.425	1.280	301.4
20.00	7.50	2331	3845.6	13.134	1.1725	1.4743	687	0.0004	2.500	381.1	3.886	1.424	335.4
40.00	3.75	2102	3613.6	1.1817	1.1957	.9713	643	0.0005	2.838	402.1	6.425	1.547	364.2
100.00	1.50	1797	3344.9	13.211	1.2221	.8356	576	0.000 9	3.296	424.8	12.637	1.677	395.0
200.00	.75	1579	3189.2	13.215	1.2367	.7671	521	0.000 1	3.662	438.9	21.191	1.758	413.9
400.00	.38	1379	3015.2	13.216	1.2500	.7520	465	0.0004	4.048	450.8	35.638	1.825	429.8
1000.00	.15	1142	2814.9	13.215	1.2682	.7111	392	0.000 5	4.593	464.7	70.952	1.898	447.0
2000.00	.08	983	2731.3	13.215	1.2829	.6825	340	0.000 0	5.039	471.7	119.341	1.943	457.6
4000.00	.04	841	2636.4	13.216	1.2954	.6576	290	0.000 5	5.523	478.4	200.371	1.981	466.6
$R = 0.800$; PERCENT FUEL = 13.60, O/F = 6.349													
1.00	150.00	3304	4586.9	13.622	1.1257	3.1245	651	0.002 2	0.000	506.9	2.121	.198	45.2
1.05	142.86	3290	4553.4	13.639	1.1255	3.1098	649	0.002 0	.295	506.9	1.440	.301	87.0
1.20	125.00	3253	4499.9	13.687	1.1249	3.0677	644	0.002 4	.572	525.2	1.440	.382	117.7
1.40	107.14	3211	4427.6	13.741	1.1244	3.0159	638	0.002 8	.781	289.3	1.051	.515	138.6
1.60	93.75	3174	4366.2	13.788	1.1240	2.9681	633	0.002 2	.927	282.4	1.005	.606	146.9
1.72	86.09	3154	4331.9	13.804	1.1237	2.9401	630	0.002 9	1.000	281.5	1.000	.652	148.9
2.00	75.00	3115	4265.3	13.865	1.1236	2.8824	624	0.002 4	1.132	283.4	1.016	.732	167.3
4.00	37.50	2935	3967.3	14.093	1.1228	2.5693	596	0.002 9	1.653	304.7	1.357	1.016	232.2
10.00	15.00	2704	3606.7	14.269	1.1267	2.0604	763	0.001'0	2.157	347.8	2.437	1.278	292.0
10.21	14.70	2699	3599.0	14.370	1.1269	2.0482	762	0.001'9	2.161	348.5	2.472	1.282	293.2
20.00	7.50	2526	3357.5	14.544	1.1254	1.6425	734	0.001'3	2.205	375.0	4.017	1.431	327.1
40.00	3.75	2338	3128.1	14.677	1.1220	1.2043	701	0.001'0	2.829	394.9	6.763	1.558	356.3
100.00	1.50	2064	2655.8	14.778	1.1840	.9242	647	0.000'1	3.246	419.2	13.610	1.678	388.1
200.00	.75	1864	2673.8	14.808	1.2009	.9793	598	0.000'8	3.778	434.4	23.116	1.765	408.0
400.00	.38	1634	2512.1	14.814	1.2228	.7593	545	0.000'9	3.955	447.3	39.667	1.859	424.9
1000.00	.15	1375	2327.4	14.816	1.2401	.6930	476	0.000'1	4.444	461.5	79.186	1.940	443.4
2000.00	.08	1199	2207.9	14.816	1.2532	.6639	417	0.000'5	4.658	470.4	134.069	1.990	455.0
4000.00	.04	1039	2103.9	14.816	1.2672	.6361	364	0.000'9	5.302	477.9	228.324	2.033	464.8
$R = 0.900$; PERCENT FUEL = 12.28, C/F = 7.143													
1.00	150.00	3336	4142.9	14.653	1.1226	3.2851	870	0.000'0	0.000	491.1	2.118	.197	45.8
1.05	142.86	3322	4120.9	14.672	1.1224	3.2273	866	0.001'9	.295	513.2	1.239	.380	84.3
1.20	125.00	3246	4061.3	14.726	1.1218	3.2247	864	0.002'9	.573	513.2	1.242	.382	89.8
1.40	107.14	3246	3993.5	14.787	1.1208	3.2263	857	0.001'1	.781	289.3	1.051	.515	117.7
1.60	93.75	3211	3932.7	14.840	1.1201	3.1977	852	0.002'2	.927	282.4	1.005	.606	138.6
1.72	86.09	3192	3904.1	14.869	1.1177	3.1843	849	0.002'8	1.000	281.5	1.000	.652	146.9
2.00	75.00	3154	3840.9	14.927	1.1170	3.1513	843	0.002'4	1.132	283.4	1.016	.732	167.3
4.00	37.50	2984	3560.2	15.193	1.1163	2.9668	818	0.002'0	1.636	304.7	1.360	1.016	225.2
10.00	15.00	2775	3219.0	15.529	1.1144	2.6406	786	0.002'0	2.161	338.0	2.457	1.279	285.5
10.21	14.70	2770	3211.8	15.536	1.1144	2.6362	786	0.001'9	2.172	338.0	2.493	1.284	284.6
20.00	7.50	2663	2981.5	15.765	1.1151	2.3278	762	0.001'9	2.510	363.2	4.082	1.434	317.9
40.00	3.75	2474	2760.3	15.981	1.1187	1.9560	737	0.001'6	2.835	385.4	6.960	1.564	346.9
100.00	1.50	2267	2492.1	16.217	1.1256	1.3985	699	0.000'0	3.238	410.9	14.385	1.709	379.0
200.00	.75	2092	2307.5	16.335	1.1258	1.0228	663						

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P _s , lb./sq. in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isonropic exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscosity, μ _μ , microns	Thermal conductivity, k, cal/(sec)·°K/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , lb/(sec)/lb	Area ratio, ε	Thrust coefficient, C _F	Specific impulse, I, lb/(sec)/lb
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	150.00	3341	3777.9	15.580	1.1217	3.1852	882	0.00295	0.000	476.5	2.118	0.000	0.0
1.05	142.86	3328	3757.1	15.607	1.1214	3.1798	880	0.00294	.295	472.2	1.050	.197	42.5
1.20	125.00	3292	3701.0	15.664	1.1206	3.1630	875	0.00291	.573	303.9	1.238	.380	81.8
1.40	107.14	3252	3637.1	15.730	1.1197	3.1421	869	0.00287	.782	272.4	1.005	.514	110.7
1.60	92.75	3217	3566.7	15.766	1.1190	3.1225	864	0.00283	.928	265.5	1.005	.606	130.3
1.72	87.13	3199	3553.1	15.817	1.1166	3.1111	861	0.00282	1.000	264.9	1.000	.650	139.8
2.00	75.00	3161	3493.4	15.860	1.1178	3.0666	856	0.00278	1.134	266.7	1.016	.731	157.3
4.00	37.50	2994	3228.9	16.167	1.1146	2.9493	831	0.00258	1.636	291.8	1.361	1.016	218.6
10.00	15.00	2789	2907.0	16.532	1.1117	2.7109	799	0.00229	4.162	328.3	2.462	1.279	275.3
10.21	14.70	2765	2900.1	16.539	1.1116	2.7047	798	0.00228	4.172	329.0	2.498	1.244	276.4
20.00	7.50	2644	2682.4	16.795	1.1106	2.6914	775	0.00205	4.251	352.8	4.097	1.434	308.7
40.00	3.75	2505	2472.8	17.043	1.1107	2.6240	752	0.00180	4.287	374.7	7.007	1.566	337.0
100.00	1.50	2325	2217.2	17.345	1.1135	1.8808	719	0.00145	3.244	400.0	14.608	1.712	368.5
200.00	.75	2188	2039.0	17.547	1.1188	1.5942	692	0.00120	3.542	416.7	25.757	1.807	389.0
400.00	.38	2048	1873.6	17.718	1.1202	1.3134	662	0.00096	3.834	431.6	45.624	1.891	407.1
1000.00	.15	1850	1674.1	17.886	1.1497	.9862	617	0.00059	4.2240	446.7	97.111	1.988	427.8
2000.00	.08	1688	1538.1	17.962	1.1732	.8015	573	0.00044	4.522	459.9	170.978	2.051	441.5
4000.00	.04	1517	1415.4	17.999	1.1980	.6640	527	0.00043	4.853	469.5	298.702	2.107	453.4
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	150.00	3219	2626.1	19.176	1.1249	1.9992	905	0.00193	0.000	421.7	2.120	0.000	0.0
1.05	142.86	3208	2609.8	19.199	1.1247	1.9899	903	0.00191	.295	268.9	1.240	.381	37.6
1.20	125.00	3169	2565.9	19.260	1.1242	1.9637	897	0.00188	.572	240.7	1.031	.515	97.9
1.40	107.14	3127	2515.9	19.330	1.1237	1.9320	891	0.00183	.781	240.7	1.005	.606	115.3
1.60	93.75	3091	2473.5	19.390	1.1233	1.9032	885	0.00180	.927	234.8	1.000	.651	123.9
1.72	86.98	3071	2449.6	19.424	1.1232	1.8866	881	0.00178	1.000	234.2	1.016	.732	139.2
2.00	75.00	3031	2403.5	19.489	1.1228	1.8526	875	0.00173	1.133	235.8	1.016	.732	139.2
4.00	37.50	2853	2197.1	19.783	1.1223	1.6765	845	0.00152	1.635	257.7	1.357	1.016	193.2
10.00	15.00	2626	1947.2	20.134	1.1249	1.4248	806	0.00123	2.158	289.4	2.439	1.278	243.0
10.21	14.70	2621	1942.0	20.141	1.1250	1.4266	805	0.00123	2.169	290.1	2.474	1.283	244.0
20.00	7.50	2455	1774.4	20.361	1.1306	1.1951	774	0.00102	2.507	310.5	4.027	1.431	272.2
40.00	3.75	2281	1614.9	20.545	1.1413	.9827	740	0.00082	2.834	324.0	6.805	1.559	296.6
100.00	1.50	2037	1424.2	20.710	1.1651	.7495	687	0.00060	3.249	349.7	13.824	1.700	325.4
200.00	.75	1842	1295.4	20.774	1.1681	.6298	641	0.00048	3.566	362.8	23.081	1.789	340.3
400.00	.38	1644	1180.0	20.802	1.2093	.5593	589	0.00040	3.903	374.0	40.495	1.865	354.7
1000.00	.15	1393	1047.4	20.811	1.2308	.5103	517	0.00033	4.391	386.3	82.105	1.948	370.6
2000.00	.08	1220	900.9	20.813	1.2441	.4869	463	0.00028	4.779	394.0	139.978	2.001	380.6
4000.00	.04	1062	885.4	20.813	1.2573	.4666	409	0.00024	5.226	400.5	238.311	2.046	389.2
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	150.00	3045	2016.0	21.610	1.1322	1.3351	900	0.00110	0.000	0.0	0.0	0.000	0.0
1.05	142.86	3031	2002.4	21.631	1.1322	1.3254	898	0.00129	.294	356.3	2.126	.198	34.4
1.20	125.00	2992	1965.5	21.688	1.1323	1.2984	891	0.00126	.571	246.4	1.242	.381	66.3
1.40	107.14	2947	1923.6	21.752	1.1326	1.2665	885	0.00122	.778	220.3	1.052	.516	89.7
1.60	93.75	2937	1886.0	21.807	1.1329	1.2351	876	0.00118	.924	214.8	1.006	.607	105.6
1.72	86.67	2886	1867.2	21.838	1.1331	1.2211	872	0.00116	1.000	214.2	1.000	.655	113.8
2.00	75.00	2845	1829.3	21.893	1.1336	1.1694	865	0.00113	1.129	215.6	1.015	.733	127.4
4.00	37.50	2649	1657.8	22.145	1.1382	1.0314	829	0.00099	1.627	235.1	1.348	1.016	176.6
10.00	15.00	2388	1451.9	22.405	1.1514	.8231	778	0.00073	2.151	263.1	2.393	1.275	221.6
10.21	14.70	2382	1447.6	22.450	1.1518	.8187	777	0.00072	2.162	263.7	2.427	1.280	222.4
20.00	7.50	2184	1311.8	22.540	1.1681	.6852	736	0.00059	2.502	281.4	3.895	1.424	247.5
40.00	3.75	1974	1185.0	22.621	1.1892	.5809	688	0.00048	2.839	297.0	6.456	1.547	268.9
100.00	1.50	1694	1037.6	22.665	1.2166	.4989	614	0.00038	3.291	313.9	16.741	1.679	291.8
200.00	.75	1492	940.9	22.675	1.2242	.4656	562	0.00032	3.652	324.5	21.403	1.760	302.9
400.00	.38	1305	856.0	22.677	1.2462	.4438	506	0.00028	4.035	333.4	36.042	1.828	317.7
1000.00	.15	1084	760.3	22.677	1.2629	.4409	434	0.00023	4.576	343.1	71.914	1.902	330.6
2000.00	.08	935	699.0	22.677	1.2798	.4053	382	0.00020	5.01	349.1	121.231	1.948	338.5
4000.00	.04	803	646.6	22.677	1.2892	.3906	334	0.00017	5.495	354.1	204.087	1.986	345.2
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	150.00	2695	1381.4	24.614	1.1581	0.7383	859	0.00072	0.000	0.0	0.0	0.000	0.0
1.05	142.86	2679	1370.8	24.628	1.1582	0.7306	856	0.00071	.291	340.3	2.145	.200	30.3
1.20	125.00	2634	1342.2	24.666	1.1609	0.7094	847	0.00069	.564	216.5	1.251	.385	58.4
1.40	107.14	2582	1309.9	24.706	1.1635	0.6854	837	0.00066	.769	193.4	1.057	.520	78.9
1.60	93.75	2537	1282.4	24.739	1.1661	0.6550	828	0.00063	.913	188.4	1.007	.612	92.8
1.72	85.58	2507	1263.9	24.760	1.1679	0.6213	824	0.00062	1.000	187.7	1.000	.666	101.1
2.00	75.00	2462	1237.6	24.789	1.1707	0.6191	813	0.00059	1.116	188.6	1.012	.737	111.9
4.00	37.50	2226	1107.7	24.905	1.1886	0.5411	762	0.00049	1.610	204.4	1.320	1.017	154.3
10.00	15.00	1914	956.0	24.980	1.2156	.4504	640	0.00039	2.142	226.7	2.271	1.267	192.3
10.21	14.70	1907	952.3	24.981	1.2161	.4575	688	0.00038	2.154	227.2	2.301	1.272	193.0
20.00	7.50	1687	857.4	25.000	1.2333	.4232	632	0.00033	2.517	240.8	3.001	1.407	213.5
40.00	3.75	1475	770.4	25.006	1.2473	.4015	574	0.00029	2.891	252.7	5.831	1.520	230.6
100.00	1.50	1224	672.4	25.000	1.2631	.3616	499	0.00024	3.397	265.4	11.232	1.637	248.4
200.00	.75	1057	604.6	25.003	1.2757	.3682	445	0.00021	3.796	273.2	18.588	1.709	255.1
400.00	.38	908	555.6	25.008	1.2875	.3559							

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OX/GEN
[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P_e , lb/in. abs	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec·°K·cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb(sec)/lb	Area ratio, ϵ	Thrust coefficient, C_T , lb(sec)/lb	Specific impulse, I , lb(sec)/lb
$R = 4,000$, PERCENT FUEL = 30.54, O/F = 31.746													
1.00	150.00	2363	1054.4	26.287	1.1944	0.5005	802	0.0004t	0.000	0.000	0.000	0.000	0.0
1.05	142.86	2344	1045.7	26.294	1.1957	0.4958	798	0.0004t	0.286	308.0	2.169	2.02	27.5
1.20	125.00	2295	1022.3	26.311	1.1994	0.4833	787	0.0004t	0.556	195.6	1.261	3.89	52.8
1.40	107.14	2238	995.9	26.324	1.2037	0.4659	774	0.0004t	0.758	174.4	1.062	5.25	71.3
1.60	93.75	2188	973.9	26.341	1.2075	0.4590	763	0.0004t	0.900	169.5	1.010	6.17	85.8
1.78	84.31	2149	956.3	26.350	1.2105	0.4509	754	0.0004t	1.000	168.7	1.000	6.60	92.4
2.00	75.00	2107	937.5	26.359	1.2138	0.4426	745	0.0004t	1.101	169.4	1.009	7.43	100.9
4.00	37.50	1859	834.0	26.391	1.2322	0.4044	685	0.0004t	1.599	162.4	1.495	1.020	138.5
10.00	15.00	1555	716.5	26.404	1.2512	0.3757	605	0.0002t	2.148	401.2	2.187	1.263	171.5
10.21	14.70	1549	714.1	26.404	1.2515	0.3752	604	0.0002t	2.160	401.5	2.215	1.267	174.1
20.00	7.50	1350	640.8	26.408	1.2629	0.3616	547	0.00025	2.539	213.0	3.431	1.397	189.7
40.00	3.75	1166	575.3	26.408	1.2739	0.3600	491	0.00022	2.928	222.9	5.506	1.504	204.2
100.00	1.50	953	502.5	26.406	1.2894	0.3553	421	0.00018	3.455	233.4	10.685	1.614	41.2
200.00	.75	814	456.5	26.406	1.3021	0.3244	372	0.00016	3.873	239.8	17.201	1.680	228.1
400.00	.38	691	417.3	26.406	1.3152	0.3140	326	0.00013	4.317	245.1	28.301	1.734	235.5
1000.00	.15	552	374.6	26.406	1.3330	0.3012	270	0.00011	4.955	250.6	54.731	1.791	243.2
2000.00	.08	463	348.1	26.406	1.3459	0.2928	232	0.00009	5.487	254.0	90.095	1.826	247.9
4000.00	.04	387	326.0	26.406	1.3563	0.2864	197	0.00007	6.075	256.8	148.169	1.854	251.7
$R = 5,000$, PERCENT FUEL = 24.58, O/F = 39.683													
1.00	150.00	2066	855.0	27.307	1.2269	0.0020	741	0.00037	0.000	0.000	0.000	0.000	0.0
1.05	142.86	2048	847.7	27.310	1.2284	0.0018	737	0.00036	0.83	282.4	1.188	2.04	25.2
1.20	125.00	1998	828.0	27.315	1.2315	0.0016	725	0.00035	549	179.0	1.269	3.92	48.4
1.40	107.14	1941	805.9	27.321	1.2353	0.0014	711	0.00034	750	159.3	1.066	5.29	65.3
1.60	93.75	1892	787.3	27.325	1.2384	0.0013	699	0.00033	891	154.8	1.011	6.22	76.7
1.80	83.45	1850	771.5	27.327	1.2410	0.0012	688	0.00032	1.000	153.9	1.000	6.90	85.2
2.00	75.00	1812	757.3	27.329	1.2433	0.0012	679	0.00032	1.092	154.4	1.007	7.47	92.2
4.00	37.50	1578	672.0	27.337	1.2563	0.0012	617	0.00028	1.594	165.7	1.281	1.022	166.2
10.00	15.00	1303	576.2	27.338	1.2708	0.3411	539	0.00023	2.152	182.2	2.144	1.262	155.7
10.21	14.70	1298	574.3	27.338	1.2711	0.3408	538	0.00023	2.164	182.5	2.171	1.266	156.3
20.00	7.50	1122	515.2	27.339	1.2815	0.3309	484	0.00020	2.550	192.6	3.343	1.393	171.9
40.00	3.75	961	462.8	27.339	1.2929	0.3209	432	0.00018	2.947	201.2	5.332	1.496	184.7
100.00	1.50	778	405.1	27.339	1.3094	0.3076	367	0.00015	3.487	210.3	10.668	1.603	197.9
200.00	.75	658	369.0	27.339	1.3227	0.2979	321	0.00012	3.919	215.8	16.403	1.666	205.6
400.00	.38	554	338.5	27.339	1.3364	0.2867	279	0.00011	4.380	220.3	26.799	1.717	212.0
1000.00	.15	438	305.6	27.339	1.3536	0.2782	229	0.00008	5.068	225.0	51.350	1.771	218.7
2000.00	.08	365	285.4	27.339	1.3632	0.2728	195	0.00007	5.612	227.8	83.996	1.803	222.6
4000.00	.04	303	268.6	27.339	1.3697	0.2693	164	0.00006	6.235	230.1	137.472	1.830	225.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Combustion-chamber pressure, 300 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P ₀ /lb/in ² abs	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c _p , cal/g/K	Viscosity, μ _μ , poise	Thermal conductivity, k, cal/sec ² K/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , lb-sec/lb	Area ratio, ε	Thrust coefficient, C _f	Specific impulse, I, lb-sec/lb
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	300.00	1183	5313.5	4.416	1.3396	1.67752	314	0.00073	0.000	0.000	0.000	0.000	0.000
1.05	285.71	1168	5287.7	4.416	1.3406	1.67710	311	0.00073	.271	530.1	2.250	.210	47.4
1.20	250.00	1129	5218.6	4.416	1.3426	1.67597	303	0.00070	.267	534.4	1.247	.03	90.6
1.40	214.29	1085	5141.9	4.416	1.3469	1.67472	293	0.00068	.262	296.1	1.081	.543	122.2
1.60	187.50	1049	5077.7	4.416	1.3497	1.67369	285	0.00066	.260	288.6	1.018	.636	143.2
1.87	160.84	1008	5006.8	4.416	1.3527	1.67257	276	0.00063	1.000	284.1	1.000	.725	163.4
2.00	150.00	989	4975.4	4.416	1.3550	1.67210	272	0.00062	1.059	284.4	1.003	.761	171.5
4.00	75.00	824	4693.4	4.416	1.3651	1.68282	234	0.00052	1.956	301.7	1.233	1.031	232.3
10.00	30.00	643	4392.5	4.416	1.3748	1.6505	188	0.00042	2.152	327.5	1.974	1.257	283.1
20.00	15.00	532	4204.8	4.416	1.3799	1.6334	159	0.00035	2.086	343.5	2.982	1.376	309.9
20.41	14.70	529	4204.9	4.416	1.3801	1.6339	158	0.00035	2.089	343.9	3.020	1.379	310.5
40.00	7.50	439	4058.9	4.416	1.3824	1.6267	133	0.00029	3.031	356.4	4.620	1.467	330.4
100.00	3.00	340	3894.0	4.416	1.3880	1.6059	104	0.00023	5.648	369.8	8.432	1.558	350.8
200.00	1.50	280	3804.5	4.416	1.3923	1.5970	85	0.00018	4.149	377.7	13.431	1.610	364.6
400.00	.75	230	3723.2	4.416	1.4004	1.5571	70	0.00012	4.675	384.1	21.488	1.652	374.0
1000.00	.30	175	3640.1	4.416	1.4132	1.4840	55	0.00011	5.437	390.6	39.928	1.694	381.6
2000.00	.15	142	3590.9	4.416	1.4151	1.4557	45	0.00009	6.076	394.3	63.572	1.719	387.2
4000.00	.08	114	3591.2	4.416	1.4171	1.4040	36	0.00007	6.843	397.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	300.00	1514	2969.7	5.216	1.3078	1.6188	402	0.00084	0.000	0.000	0.000	0.000	0.000
1.05	285.71	1497	2941.7	5.216	1.3099	1.6144	399	0.00083	.274	554.2	2.233	.209	49.3
1.20	250.00	1450	2866.8	5.216	1.3119	1.6082	389	0.00081	.253	348.6	1.289	.000	94.6
1.40	214.29	1398	2783.2	5.216	1.3154	1.5889	378	0.00078	.270	309.3	1.077	.339	127.4
1.60	187.50	1354	2715.2	5.216	1.3165	1.5773	369	0.00076	.869	299.6	1.016	.632	149.4
1.85	162.47	1307	2640.5	5.216	1.3217	1.5652	359	0.00073	1.000	297.3	1.000	.716	169.2
2.00	150.00	1282	2601.1	5.216	1.3235	1.5568	359	0.00072	1.058	297.8	1.004	.757	179.1
4.00	75.00	1079	2290.0	5.216	1.3391	1.5056	207	0.00061	1.572	316.7	1.244	1.029	243.2
10.00	30.00	856	1954.3	5.216	1.3559	1.4516	251	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	15.00	709	1746.8	5.216	1.3626	1.4232	213	0.00040	2.573	362.0	3.049	1.379	325.9
20.41	14.70	705	1743.2	5.216	1.3628	1.4222	212	0.00040	2.586	362.4	3.088	1.382	326.7
40.00	7.50	588	1578.0	5.216	1.3715	1.4065	179	0.00034	3.010	376.0	4.739	1.672	348.0
100.00	3.00	458	1296.3	5.216	1.3771	1.3915	142	0.00026	3.619	390.5	8.679	1.665	370.0
200.00	1.50	379	1286.1	5.216	1.3811	1.3807	117	0.00022	4.111	399.1	13.870	1.619	382.7
400.00	.75	312	1195.2	5.216	1.3801	1.3677	96	0.00018	4.638	406.1	22.296	1.662	393.0
1000.00	.30	242	1098.9	5.216	1.3912	1.3402	74	0.00013	5.394	413.4	41.979	1.706	403.5
2000.00	.15	198	1041.1	5.216	1.4126	1.2977	61	0.00011	6.014	417.7	67.687	1.733	409.7
4000.00	.08	161	995.9	5.216	1.4126	1.2571	50	0.00009	6.705	421.1	108.755	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	300.00	1817	1249.3	6.016	1.2824	1.5015	481	0.00092	0.000	0.000	0.000	0.000	0.000
1.05	285.71	1797	1220.2	6.016	1.2835	1.4971	477	0.00091	.276	563.4	2.218	.207	50.3
1.20	250.00	1745	1142.1	6.016	1.2883	1.4852	467	0.00089	.258	556.2	1.283	.398	96.6
1.40	214.29	1686	1054.7	6.016	1.2895	1.4719	456	0.00086	.736	318.3	1.073	.536	130.1
1.60	187.50	1626	981.45	6.016	1.2923	1.4660	446	0.00084	.876	306.6	1.015	.629	152.7
1.83	164.91	1587	909.9	6.016	1.2931	1.4498	436	0.00081	1.000	304.7	1.000	.708	171.8
2.00	150.00	1555	863.9	6.016	1.2971	1.4425	429	0.00080	1.076	305.1	1.005	.754	183.1
4.00	75.00	1322	535.1	6.016	1.3125	1.3875	378	0.00068	1.578	325.5	1.256	1.027	249.3
10.00	30.00	1057	176.1	6.016	1.3329	1.3226	314	0.00054	2.147	355.3	2.048	1.258	305.6
20.00	15.00	887	954.0	6.016	1.3400	1.2849	269	0.00046	2.563	373.7	3.127	1.384	335.7
20.41	14.70	852	9246.0	6.016	1.3404	1.2838	268	0.00042	2.575	374.2	3.166	1.386	336.5
40.00	7.50	741	9786.1	6.016	1.3508	1.2560	228	0.00038	2.987	388.7	4.883	1.478	359.0
100.00	3.00	581	9569.0	6.016	1.3663	1.2321	181	0.00030	3.281	404.4	8.985	1.574	382.4
200.00	1.50	482	9447.8	6.016	1.3716	1.2192	191	0.00025	4.064	413.4	14.396	1.630	395.9
400.00	.75	399	9347.3	6.016	1.3755	1.2099	125	0.00020	4.581	420.9	23.208	1.675	406.8
1000.00	.30	310	9240.5	6.016	1.3820	1.1949	97	0.00015	5.327	428.7	43.894	1.722	418.1
2000.00	.15	256	9175.9	6.016	1.3867	1.1801	78	0.00012	5.945	435.4	71.280	1.749	424.7
4000.00	.08	210	9122.7	6.016	1.3942	1.1475	64	0.00010	6.605	437.2	115.650	1.771	430.2
R = 0.300, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	300.00	2093	9932.47	6.814	1.2600	1.4230	550	0.00098	0.000	0.000	0.000	0.000	0.000
1.05	285.71	2072	9703.1	6.814	1.2611	1.4174	547	0.00097	.279	568.5	2.206	.206	50.8
1.20	250.00	2016	9623.5	6.815	1.2640	1.4024	537	0.00095	.542	359.8	1.277	.396	97.5
1.40	214.29	1952	9734.4	6.815	1.2674	1.3865	529	0.00092	.742	319.8	1.070	.533	131.4
1.60	187.50	1877	9595.4	6.815	1.2702	1.3740	515	0.00090	.882	310.5	1.013	.626	154.2
1.82	162.12	1866	9590.1	6.816	1.2729	1.3623	503	0.00087	1.000	308.3	1.000	.701	172.7
2.00	150.00	1809	9336.9	6.816	1.2750	1.3323	498	0.00086	1.082	309.1	1.000	.751	185.1
4.00	75.00	1553	9199.7	6.816	1.2893	1.2994	442	0.00074	1.585	330.6	1.266	1.025	252.6
10.00	30.00	1257	8825.3	6.816	1.3095	1.2336	373	0.00060	2.148	361.8	2.085	1.260	310.4
20.00	15.00	1054	8591.2	6.816	1.3248	1.1891	325	0.00021	2.555	381.2	3.206	1.386	341.7
20.41	14.70	1059	8584.9	6.816	1.3273	1.1878	324	0.00020	2.567	381.7	3.248	1.390	342.5
40.00	7.50	895	8393.6	6.816	1.3384	1.1531	279	0.00042	2.968	397.0	5.037	1.485	366.0
100.00	3.00	707	8180.4	6.816	1.3551	1.1173	223	0.00035	3.544	413.5	9.325	1.584	390.5
200.00	1.50	570	8049.6	6.816	1.3603	1.1006	187	0.00027	4.013	423.3	14.993	1.642	404.8
400.00	.75	470	7740.5	6.816	1.3667	1.0665	156	0.0002					

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/in. ² abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, Y	Specific heat, C _p , cal/(lb·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb/sec)/lb	Area ratio, ε	Thrust coefficient, C _T	Specific impulse, I, sec/lb
R = 0.350+, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	300.00	2344	8892.8	7.607	1.2379	1.3936	610	0.00105	0.000	0.281	569.6	2.194	0.000 0.0
1.05	285.71	2322	8863.0	7.608	1.2391	1.3850	507	0.00104	.281	569.6	2.194	2.02	50.9
1.20	250.00	2263	8783.1	7.610	1.2425	1.3629	597	0.00101	.547	360.9	1.272	3.93	97.7
1.40	214.29	2196	8593.4	7.611	1.2463	1.3398	586	0.00098	.747	321.1	1.066	.531	131.7
1.60	187.50	2139	8617.8	7.612	1.2495	1.3219	576	0.00097	.888	311.7	1.012	.623	154.7
1.80	166.26	2088	8551.5	7.613	1.2523	1.3072	567	0.00093	1.000	307.9	1.000	.654	172.3
2.00	150.00	2045	8496.0	7.614	1.2546	1.2922	559	0.00091	1.089	310.8	1.007	.746	165.8
4.00	75.00	1771	8151.2	7.616	1.2675	1.2410	506	0.00079	1.590	333.4	1.275	1.043	254.0
10.00	30.00	1451	7766.9	7.616	1.2804	1.1607	434	0.00065	2.149	362.6	2.119	1.261	313.0
20.00	15.00	1248	7524.1	7.616	1.3035	1.1402	381	0.00052	2.545	382.8	3.281	1.390	345.1
20.41	14.70	1232	7517.5	7.616	1.3040	1.1192	379	0.00053	2.561	380.4	3.325	1.393	345.1
40.00	7.50	1051	7317.5	7.616	1.3168	1.0794	330	0.00046	2.952	402.4	5.189	1.491	370.2
100.00	3.00	838	7092.6	7.616	1.3368	1.0363	267	0.00036	3.511	419.8	9.678	1.594	395.8
200.00	1.50	702	6953.6	7.616	1.3474	1.0113	225	0.00030	3.964	430.2	15.630	1.654	410.8
400.00	.75	586	6837.4	7.616	1.3553	.9954	169	0.00025	4.453	438.6	25.355	1.703	422.9
1000.00	.30	460	5712.9	7.616	1.3553	.9791	148	0.00019	5.161	447.5	48.296	1.754	435.5
2000.00	.15	382	5636.9	7.616	1.3564	.9692	121	0.00016	5.751	452.6	78.866	1.784	435.5
4000.00	.08	317	5673.9	7.616	1.3733	.9596	96	0.00013	6.392	457.2	128.975	1.809	449.2
R = 0.400+, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	300.00	2565	8050.5	8.389	1.2157	1.4207	662	0.00114	0.000	0.284	567.8	2.181	0.000 0.0
1.05	285.71	2543	8021.0	8.390	1.2170	1.4084	658	0.00112	.284	567.8	2.181	.204	50.9
1.20	250.00	2484	7941.5	8.395	1.2205	1.3764	649	0.00109	.521	360.1	1.267	.391	97.7
1.40	214.29	2417	7852.1	8.399	1.2247	1.3423	638	0.00105	.753	320.7	1.065	.528	131.7
1.60	187.50	2359	7776.7	8.403	1.2283	1.3193	629	0.00101	.894	311.6	1.011	.620	154.7
1.79	167.44	2310	7714.6	8.405	1.2313	1.2941	621	0.00099	1.000	310.0	1.000	.687	171.1
2.00	150.00	2263	7654.6	8.407	1.2342	1.2792	613	0.00096	1.095	311.0	1.008	.746	185.6
4.00	75.00	1978	7307.8	8.414	1.2500	1.1857	561	0.00083	1.594	334.2	1.285	1.021	254.2
10.00	30.00	1637	6917.4	8.416	1.2648	1.1119	489	0.00069	2.148	361.6	2.152	1.262	314.0
20.00	15.00	1409	6668.4	8.416	1.2682	1.0671	434	0.00059	2.544	388.5	3.356	1.393	346.8
20.41	14.70	1403	6661.6	8.416	1.2686	1.0658	433	0.00059	2.555	389.1	3.399	1.397	347.6
40.00	7.50	1205	6454.8	8.416	1.2991	1.0255	380	0.00050	2.939	405.6	5.336	1.497	372.6
100.00	3.00	970	6220.2	8.416	1.3188	.9760	313	0.00040	3.480	424.1	10.038	1.603	399.1
200.00	1.50	819	6074.1	8.416	1.3191	.9478	266	0.00033	3.919	435.0	16.294	1.666	414.7
400.00	.75	687	5951.2	8.416	1.3428	.9290	224	0.00027	4.390	443.9	26.545	1.717	427.4
1000.00	.30	542	5818.7	8.416	1.3557	.9038	176	0.00021	5.074	453.3	50.799	1.770	440.7
2000.00	.15	452	5737.5	8.416	1.3595	.8829	146	0.00017	5.646	459.0	83.167	1.802	448.6
4000.00	.08	376	5670.0	8.416	1.3650	.8831	119	0.00014	6.269	463.6	136.362	1.829	455.1
R = 0.450+, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	300.00	2755	7354.5	9.152	1.1932	1.5003	705	0.00125	0.000	0.286	563.0	2.169	0.000 0.0
1.05	285.71	2734	7325.4	9.155	1.1960	1.4843	702	0.00123	.286	563.0	2.169	.204	50.9
1.20	250.00	2677	7247.0	9.164	1.1979	1.4419	693	0.00119	.556	357.9	1.261	.389	96.7
1.40	214.29	2611	7158.7	9.173	1.2026	1.3959	683	0.00114	.758	319.1	1.062	.525	130.5
1.60	187.50	2555	7084.0	9.180	1.2072	1.3586	675	0.00110	.900	310.4	1.010	.617	155.4
1.78	168.67	2510	7026.0	9.185	1.2100	1.3312	668	0.00107	1.000	308.8	1.000	.680	169.1
2.00	150.00	2460	6962.9	9.190	1.2132	1.3023	660	0.00104	1.102	310.0	1.009	.743	184.6
4.00	75.00	2173	6616.3	9.208	1.2319	1.1697	610	0.00084	1.599	333.9	1.295	1.020	255.4
10.00	30.00	1818	6222.5	9.215	1.2529	1.0717	540	0.00072	2.147	368.2	2.187	1.263	313.8
20.00	15.00	1576	5969.2	9.216	1.2667	1.0246	485	0.00063	2.537	389.8	3.427	1.397	347.2
20.41	14.70	1569	5962.6	9.216	1.2671	1.0233	483	0.00063	2.548	390.3	3.474	1.401	348.1
40.00	7.50	1356	5750.2	9.216	1.2810	.9831	430	0.00054	2.942	407.7	5.487	1.503	373.6
100.00	3.00	1105	5507.6	9.216	1.3007	.9527	358	0.00043	3.453	426.7	10.491	1.613	400.9
200.00	1.50	938	5355.2	9.216	1.3121	.8999	308	0.00030	3.877	438.4	16.963	1.676	417.1
400.00	.75	793	5226.1	9.216	1.3281	.8728	261	0.00030	4.331	447.6	27.800	1.732	430.3
1000.00	.30	630	5082.2	9.216	1.3418	.8485	207	0.00023	4.990	457.6	53.499	1.780	444.3
2000.00	.15	527	5000.0	9.216	1.3501	.8315	174	0.00019	5.541	463.6	87.879	1.821	452.6
4000.00	.08	440	4927.9	9.216	1.3501	.8211	142	0.00016	6.144	468.5	144.468	1.849	459.5
R = 0.500+, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	300.00	2915	6769.6	9.891	1.1779	1.6231	741	0.00139	0.000	0.286	557.9	2.158	0.000 0.0
1.05	285.71	2895	6741.2	9.897	1.1788	1.6040	738	0.00137	.286	557.9	2.158	.201	49.8
1.20	250.00	2841	6664.3	9.911	1.1814	1.5535	730	0.00132	.559	354.6	1.256	.387	95.7
1.40	214.29	2778	6577.6	9.926	1.1847	1.4970	721	0.00126	.764	316.4	1.080	.523	129.3
1.60	187.50	2724	6500.1	9.938	1.1878	1.4902	713	0.00121	.906	307.9	1.009	.615	156.0
1.77	169.85	2684	6450.6	9.946	1.1901	1.4168	707	0.00118	1.000	306.6	1.000	.674	166.6
2.00	150.00	2633	6384.7	9.956	1.1932	1.3700	699	0.00114	1.108	307.7	1.010	.740	183.0
4.00	75.00	2352	6040.6	9.993	1.2121	1.1932	654	0.00094	1.604	332.6	1.307	1.019	251.9
10.00	30.00	1992	5645.6	10.012	1.2359	1.0200	587	0.00076	2.145	367.7	2.244	1.265	316.7
20.00	15.00	1740	5389.3	10.015	1.2509	.9916	553	0.00066	2.529	389.9	3.204	1.401	346.6
20.41	14.70	1732	5382.2	10.015	1.2513	.9902	551	0.00066	2.549	390.4	3.253	1.402	347.5
40.00	7.50	1509	5166.1	10.016	1.2644	.9941	477	0.00057	2.910	408.4	9.642	1.511	373.5
100.00	3.00	1240	4916.8	10.016	1.2833	.8898	404	0.00046	3.427	428.2	10.777	1.624	401.5
200.00	1.50	1060	4758.9	10.016	1.2982	.8628	350	0.00039	3.837	440.2	17.699	1.691	416.3
400.00	.75	902	4624.2	10.016	1.3123	.8336	300	0.00032</					

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s , lb/in ²	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec·°K·cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/(lb·sec)	Area ratio, ϵ	Thrust coefficient, C_F	Specific impulse, I , lb/(sec/lb)
$R = 0.600$, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	300.00	3155	5841.6	11.290	1.1529	1.9667	796	0.00174	0.000	0.000	0.000	0.000	0.0
1.05	285.71	3137	5814.6	11.300	1.1532	1.9446	794	0.00172	.291	543.6	2.140	.200	48.5
1.20	250.00	3089	5741.6	11.326	1.1544	1.8842	787	0.00166	.565	346.0	1.248	.384	93.3
1.40	214.29	3033	5658.9	11.354	1.1560	1.8145	780	0.00159	.772	309.3	1.056	.519	126.1
1.60	187.50	2985	5588.7	11.378	1.1576	1.7545	773	0.00152	.916	301.2	1.007	.611	148.4
1.75	171.73	2953	5543.1	11.393	1.1588	1.7154	768	0.00149	1.000	300.2	1.000	.663	161.2
2.00	150.00	2904	5474.1	11.415	1.1608	1.6559	761	0.00143	1.119	301.8	1.013	.736	178.8
4.00	75.00	2652	5140.3	11.510	1.1743	1.3747	724	0.00115	1.615	327.7	1.328	1.017	247.0
10.00	30.00	2311	4749.0	11.583	1.1992	1.0584	667	0.00088	2.144	364.3	2.303	1.269	308.3
20.00	15.00	2054	4489.8	11.600	2.1285	0.9752	618	0.00073	2.112	387.6	3.673	1.412	343.0
20.41	14.70	2047	4482.6	11.607	2.1290	0.9726	616	0.00073	2.122	388.2	3.726	1.416	343.9
40.00	7.50	1808	4260.9	11.614	2.1236	0.9053	565	0.00063	2.877	407.2	5.977	1.527	370.9
100.00	3.00	1512	4001.1	11.616	1.2523	.8996	492	0.00052	3.371	428.3	11.578	1.667	400.2
200.00	1.50	1311	3834.0	11.616	1.2659	0.8145	436	0.00045	3.761	441.3	19.216	1.721	418.0
400.00	.75	1130	3689.5	11.616	1.2802	0.7815	381	0.00038	4.171	452.2	31.993	1.781	432.7
1000.00	.30	919	3529.3	11.616	1.2993	.7427	312	0.00030	4.757	463.8	62.803	1.847	448.6
2000.00	.15	782	3426.8	11.616	1.3126	.7183	265	0.00025	5.244	470.9	104.524	1.886	458.2
4000.00	.08	661	3343.2	11.616	1.3242	.6988	223	0.00020	5.776	476.8	173.763	1.919	466.3
$R = 0.700$, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	300.00	3307	5138.3	12.574	1.1378	2.3992	836	0.00217	0.000	0.000	0.000	0.000	0.0
1.05	285.71	3291	5112.9	12.568	1.1378	2.3785	834	0.00215	.293	527.6	2.129	.198	47.0
1.20	250.00	3248	5044.0	12.625	1.1579	2.3020	828	0.00208	.569	336.2	1.244	.382	90.6
1.40	214.29	3178	4966.0	12.667	1.1382	2.2512	821	0.00201	.777	300.7	1.023	.517	122.4
1.60	187.50	3156	4699.5	12.702	1.1386	2.1898	818	0.00194	.922	293.1	1.006	.608	144.1
1.73	172.98	3120	4659.9	12.723	1.1389	2.1520	811	0.00190	1.000	292.3	1.000	.657	155.6
2.00	150.00	3085	4790.8	12.759	1.1395	2.0841	805	0.00183	1.127	294.1	1.014	.734	173.9
4.00	75.00	2865	4471.7	12.920	1.1454	1.7441	774	0.00150	1.625	320.4	1.344	1.016	240.8
10.00	30.00	2569	4091.1	13.081	1.1620	1.3258	728	0.00110	2.149	358.1	2.374	1.274	301.9
20.00	15.00	2345	3833.6	13.157	1.1611	1.0849	687	0.00088	2.503	382.5	3.843	1.422	336.9
20.41	14.70	2328	3826.4	13.159	1.1617	1.0791	686	0.00087	2.513	383.1	3.900	1.426	337.9
40.00	7.50	2095	3692.0	13.196	1.2020	0.9294	641	0.00072	2.846	403.2	6.337	1.543	365.6
100.00	3.00	1785	3334.7	13.213	1.2246	.8253	573	0.00058	3.312	425.6	12.441	1.672	396.1
200.00	1.50	1566	3160.2	13.216	1.2378	.7835	518	0.00050	3.682	439.6	20.858	1.751	414.9
400.00	.75	1368	3007.3	13.216	1.2508	.7500	462	0.00043	4.070	451.4	35.080	1.817	430.6
1000.00	.30	1133	2355.4	13.216	1.2670	.7094	389	0.00035	4.616	464.2	69.841	1.889	447.6
2000.00	.15	975	2725.7	13.216	1.2833	.6811	337	0.00029	5.065	472.1	117.461	1.933	458.2
4000.00	.08	834	2631.6	13.216	1.2972	.6564	288	0.00024	5.551	478.7	197.192	1.971	467.0
$R = 0.800$, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	300.00	3393	4586.9	13.740	1.1296	2.7921	864	0.00257	0.000	0.000	0.000	0.000	0.0
1.05	285.71	3378	4563.0	13.757	1.1294	2.7781	861	0.00255	.294	511.3	2.123	.198	45.6
1.20	250.00	3338	4498.3	13.803	1.1289	2.7382	856	0.00250	.571	326.0	1.241	.381	87.8
1.40	214.29	3292	4424.9	13.855	1.1284	2.6891	850	0.00244	.780	291.8	1.052	.515	118.7
1.60	187.50	3253	4362.3	13.900	1.1281	2.6439	844	0.00238	.925	284.5	1.005	.607	139.8
1.73	173.68	3231	4326.9	13.926	1.1279	2.6168	831	0.00235	1.000	283.8	1.000	.653	150.4
2.00	150.00	3169	4259.9	13.974	1.1276	2.5628	835	0.00229	1.131	285.6	1.015	.732	168.7
4.00	75.00	2995	3957.6	14.193	1.1277	2.2689	807	0.00197	1.632	312.0	1.354	1.016	234.0
10.00	30.00	2744	3592.8	14.449	1.1332	1.8019	770	0.00152	2.156	349.9	2.423	1.277	294.1
20.00	15.00	2550	3314.8	14.605	1.1439	1.4368	738	0.00119	2.505	375.0	3.982	1.429	329.1
20.41	14.70	2544	3334.7	14.609	1.1443	1.4265	737	0.00118	2.515	375.7	4.042	1.433	330.1
40.00	7.50	2344	3111.8	14.716	1.1620	1.1265	702	0.00091	2.832	396.7	6.676	1.555	358.3
100.00	3.00	2053	2840.4	14.791	1.1918	.8717	645	0.00067	3.260	420.6	13.365	1.692	389.8
200.00	1.50	1830	2659.7	14.810	1.2106	.7805	595	0.00056	3.601	435.6	22.652	1.778	409.5
400.00	.75	1617	2494.6	14.815	1.2246	.7331	541	0.00049	3.964	448.3	38.453	1.850	426.2
1000.00	.30	1360	2316.9	14.816	1.2412	.6903	468	0.00040	4.478	462.3	77.533	1.929	444.4
2000.00	.15	1185	2198.7	14.816	1.2593	.6615	413	0.00034	4.894	471.0	131.747	1.979	455.9
4000.00	.08	1027	2096.0	14.816	1.2683	.6339	359	0.00029	5.340	478.4	223.495	2.021	465.6
$R = 0.900$, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	300.00	3430	4142.9	14.789	1.1261	2.9626	883	0.00276	0.000	0.000	0.000	0.000	0.0
1.05	285.71	3416	4120.5	14.869	1.1258	2.9553	881	0.00275	.295	495.7	2.121	.198	44.2
1.20	250.00	3377	4059.8	14.861	1.1250	2.9343	875	0.00271	.572	316.0	1.240	.381	85.1
1.40	214.29	3334	3990.7	14.921	1.1242	2.9078	869	0.00267	.781	284.9	1.051	.515	115.1
1.60	187.50	3296	3931.9	14.972	1.1235	2.8830	864	0.00263	.927	276.0	1.005	.606	135.5
1.73	173.98	3276	3899.3	15.001	1.1232	2.8682	861	0.00261	1.000	275.3	1.000	.651	145.6
2.00	150.00	3235	3835.4	15.058	1.1222	2.8374	855	0.00257	1.133	277.1	1.016	.732	163.6
4.00	75.00	3054	3550.3	15.317	1.1198	2.6636	829	0.00236	1.635	303.0	1.358	1.016	227.1
10.00	30.00	2276	2472.2	16.273	1.1185	2.5536	795	0.00100	2.161	340.5	2.448	1.278	285.8
20.00	15.00	2666	2964.3	15.867	1.1199	2.0547	769	0.00170	2.511	365.6	4.058	1.432	320.2
20.41	14.70	2661	2957.5	15.873	1.1200	2.0450	768	0.00169	2.521	366.3	4.121	1.437	321.2
40.00	7.50	2403	2741.4	16.068	1.1233	1.7023	742	0.00138	2.827	387.8	6.901	1.562	349.2
100.00	3.00	2276	2472.2	16.273	1.1185	1.2030	700	0.00095	3.241	413.0	14.187	1.706	381.3
200.00	1.50	2084	2288.0	16.364	1.1189								

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/in ² atm	Temp., T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/g-K°	Viscosity, μ, poises	Thermal conductivity, k, cal/sec·K·cm	Mach number, M	Specific impulse in vacuum, I _{vac} , sec	Area ratio, E	Thrust coefficient, C _f	Specific impulse, I, lb-sec/lb
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	300.00	3437	3777.9	15.734	1.1250	2.8811	856	0.00272	0.000			0.000	0.0
1.05	285.71	3423	3756.8	15.755	1.1247	2.8760	854	0.00271	2.429	481.0	2.120	.198	42.9
1.20	250.00	3584	3694.5	15.811	1.1239	2.8601	850	0.00268	5.74	508.7	1.239	.380	62.6
1.40	214.29	3561	3634.5	15.845	1.1230	2.8421	842	0.00265	17.81	274.6	1.021	.915	111.7
1.60	187.50	3304	3579.1	15.930	1.1222	2.8243	837	0.00261	59.27	267.9	1.002	.666	131.3
1.72	174.06	3284	3546.5	15.961	1.1218	2.8158	834	0.00259	19.00	267.2	1.000	.651	141.3
2.00	150.00	3244	3488.2	16.023	1.1211	2.7914	828	0.00256	16.133	264.0	1.016	.732	156.8
4.00	75.00	3065	3219.4	16.303	1.1179	2.6657	842	0.00247	16.35	294.2	1.459	1.010	220.4
10.00	30.00	2847	2893.0	16.659	1.1121	2.4459	806	0.0020	2.162	330.7	2.453	1.279	477.5
20.00	15.00	2692	2656.5	16.914	1.1142	2.4551	783	0.0017	2.512	355.3	4.076	1.453	511.1
20.41	14.70	2667	2659.2	16.921	1.1142	2.4567	783	0.0017	2.522	356.0	4.140	1.458	512.0
40.00	7.50	2542	2645.2	1.1148	2.0143	758	0.0014	2.840	377.1	6.959	1.564	339.4	
100.00	3.00	2349	2196.7	17.439	1.1186	1.0051	724	0.0012	3.250	402.3	14.469	1.709	370.9
200.00	1.50	2203	2017.9	17.625	1.1200	1.0246	691	0.0019	3.549	416.9	25.442	1.883	391.3
400.00	.75	2054	1654.3	17.779	1.1206	1.0170	603	0.0007	3.842	433.7	44.922	1.886	407.3
1000.00	.30	1839	1653.8	17.920	1.1274	.9997	614	0.0004	4.239	450.6	95.113	1.981	429.9
2000.00	.15	1668	1519.2	17.979	1.1281	.7520	700	0.0001	4.553	461.4	166.760	2.093	443.3
4000.00	.08	1493	1398.2	18.005	1.2043	.6600	520	0.0002	4.897	470.8	290.406	2.097	455.0
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	300.00	3297	2626.1	19.320	1.1288	1.8003	918	0.00177	0.000			0.000	0.0
1.05	285.71	3282	2609.6	19.342	1.1286	1.7919	915	0.00176	2.294	425.1	2.123	.198	37.9
1.20	250.00	3243	2564.9	19.401	1.1281	1.7680	908	0.00172	5.71	271.0	1.241	.381	75.0
1.40	214.29	3158	2514.1	19.466	1.1277	1.7591	904	0.0018	7.80	242.6	1.052	.515	98.7
1.60	187.50	3159	2470.9	19.526	1.1273	1.7131	906	0.0015	9.29	236.6	1.005	.607	116.2
1.72	173.72	3127	2466.4	19.558	1.1271	1.6977	902	0.0013	1.000	239.4	1.000	.655	125.0
2.00	150.00	3056	2400.0	19.620	1.1269	1.6674	886	0.0019	1.151	237.5	1.015	.732	140.2
4.00	75.00	2944	2190.9	19.900	1.1267	1.5076	854	0.0019	1.652	259.4	1.354	1.016	194.6
10.00	30.00	2661	1938.5	20.228	1.1304	1.2677	812	0.0013	2.150	291.1	2.427	1.217	244.6
20.00	15.00	2478	1764.5	20.435	1.1369	1.0774	779	0.0003	3.028	312.1	3.997	1.449	273.8
20.41	14.70	2472	1759.5	20.440	1.1372	1.0719	778	0.0003	3.516	312.7	4.056	1.434	274.6
40.00	7.50	2221	1604.4	20.597	1.1487	.8963	742	0.0005	4.837	330.4	6.734	1.557	298.2
100.00	3.00	2024	1413.9	20.734	1.1746	.7030	686	0.0006	3.250	350.9	13.621	1.665	324.8
200.00	1.50	1858	1285.8	20.784	1.1958	.6070	638	0.0006	3.582	363.8	25.271	1.783	341.5
400.00	.75	1629	1171.3	20.805	1.2116	.5200	582	0.0009	3.927	374.8	39.732	1.857	355.8
1000.00	.30	1379	1039.8	20.812	1.2343	.2074	513	0.0004	4.422	386.9	80.499	1.940	371.5
2000.00	.15	1297	954.3	20.813	1.2424	.4830	458	0.0004	4.828	394.5	137.14	1.991	381.4
4000.00	.08	1050	879.8	20.812	1.2584	.4690	402	0.0004	5.463	401.0	235.567	2.035	389.8
R = 2.000, PERCENT FULL = 5.927, O/F = 15.873													
1.00	300.00	3103	2026.0	21.723	1.1368	1.2138	910	0.0011	0.000			0.000	0.0
1.05	285.71	3088	2002.4	21.743	1.1368	1.2052	907	0.0010	2.93	388.8	2.129	.198	34.7
1.20	250.00	3046	1954.8	21.797	1.1370	1.1812	900	0.0017	5.569	247.8	1.243	.382	66.7
1.40	214.29	2998	1922.4	21.857	1.1373	1.1526	892	0.0013	7.77	221.6	1.053	.517	90.2
1.60	187.50	2957	1886.3	21.908	1.1377	1.1476	885	0.0010	9.22	216.1	1.006	.606	106.2
1.72	173.72	2932	1854.9	21.938	1.1380	1.1122	881	0.0018	1.000	215.4	1.000	.656	114.7
2.00	150.00	2889	1827.3	21.990	1.1381	1.0844	873	0.0015	1.147	216.8	1.014	.734	126.2
4.00	75.00	2679	1653.8	22.119	1.1439	.9449	835	0.0008	1.526	230.2	1.344	1.016	177.5
10.00	30.00	2402	1466.7	22.451	1.1579	.7034	781	0.0008	2.151	264.1	2.4279	1.217	222.6
20.00	15.00	2188	1306.3	22.567	1.1740	.6477	736	0.0006	2.502	282.4	3.681	1.422	248.5
20.41	14.70	2181	1302.4	22.569	1.1751	.6447	732	0.0005	2.515	284.7	3.918	1.426	249.2
40.00	7.50	1970	1179.6	22.633	1.1949	.5611	687	0.0006	2.846	297.7	6.385	1.544	269.8
100.00	3.00	1686	1032.8	22.668	1.2192	.4925	616	0.0007	3.204	314.5	12.580	1.674	294.5
200.00	1.50	1493	936.0	22.675	1.2341	.4634	559	0.0002	3.668	324.9	21.125	1.756	306.5
400.00	.75	1297	852.3	22.677	1.2470	.4427	503	0.0008	4.053	335.7	35.572	1.821	318.2
1000.00	.30	1076	757.2	22.677	1.2636	.4201	432	0.0003	4.596	343.4	70.973	1.894	331.0
2000.00	.15	929	656.4	22.677	1.2765	.4046	380	0.0005	5.040	349.5	119.641	1.940	338.9
4000.00	.08	797	644.1	22.677	1.2898	.3900	331	0.0007	5.518	354.3	201.392	1.978	345.5
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	300.00	2723	1381.4	24.669	1.1659	0.6709	862	0.0008	0.000			0.000	0.0
1.05	285.71	2702	1370.7	24.686	1.1646	0.6042	861	0.0008	2.90	341.6	2.146	.200	30.5
1.20	250.00	2658	1341.9	24.715	1.1667	.6659	852	0.0005	5.63	217.5	1.222	.385	58.6
1.40	214.29	2604	1309.3	24.751	1.1694	.6451	841	0.0003	7.78	194.0	1.058	.521	79.2
1.60	187.50	2556	1281.7	24.780	1.1719	.6275	834	0.0001	9.11	188.9	1.008	.613	93.1
1.72	170.82	2523	1266.7	24.798	1.1738	.6155	825	0.0009	1.000	188.4	1.000	.666	101.6
2.00	150.00	2477	1236.7	24.823	1.1766	.5591	816	0.0007	1.114	189.1	1.012	.738	114.2
4.00	75.00	2232	1106.4	24.922	1.1930	.5216	764	0.0007	1.609	204.8	1.317	1.018	154.7
10.00	30.00	1914	955.2	24.985	1.2185	.4517	690	0.0008	2.144	227.0	2.261	1.667	194.6
20.00	15.00	1684	856.1	25.002	1.2347	.4206	632	0.0003	2.521	241.0	3.584	1.408	213.8
20.41	14.70	1678	853.3	25.002	1.2351	.4199	630	0.0003	2.532	241.4	3.634	1.410	214.4
40.00	7.50	1472	769.2	25.007	1.2476	.4007	573	0.0009	2.896	252.9	5.042	1.516	250.8
100.00	3.00	1224	671.4	25.008	1.2655	.3813	498	0.0004	3.403	265.6	11.177	1.637	248.6
200.00	1.50	1055	608.7	25.008	1.2754	.3880	444	0.0001	3.802	273.4	18.498	1.707	259.3
400.00	.75	906	554.8	25.008	1.2877	.3557	393	0.0018	4.223	279.9	30.718	1.764	268.2
1000.00	.30	735	495										

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P, lb/in. ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/sec/m/K/cm	Mach number, M	Specific impulse in vacuum, I _{sp} , sec	Area ratio, ε	Thrust coefficient, C _T	Specific impulse, I, lb/sec/lb
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	300.00	2372	1054.4	26.307	1.1993	0.4836	804	0.00046	0.000			0.000	0.0
1.05	285.71	2354	1045.7	26.312	1.2005	0.4796	800	0.00046	0.466	505.2	2.172	0.403	27.5
1.20	250.00	2303	1022.2	26.327	1.2040	0.4609	789	0.00044	0.555	195.6	1.464	0.390	52.9
1.40	214.29	2244	995.8	26.341	1.2080	0.4574	776	0.00043	0.597	174.0	1.063	0.26	71.4
1.60	187.50	2194	973.4	26.352	1.2115	0.4481	765	0.00041	0.899	167.7	1.010	0.18	63.9
1.78	168.42	2153	955.8	26.360	1.2143	0.4412	755	0.00040	1.000	168.9	1.000	0.084	92.6
2.00	150.00	2110	937.2	26.367	1.2173	0.4341	745	0.00039	1.100	169.5	1.009	0.745	101.0
4.00	75.00	1859	833.7	26.394	1.2230	0.4010	685	0.00034	1.599	182.7	1.294	1.020	138.6
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	300.00	2069	855.0	27.313	1.2295	0.3968	742	0.00036	0.000			0.000	0.0
1.05	285.71	2051	847.7	27.315	1.2306	0.3947	737	0.00036	0.282	482.5	2.189	0.204	25.2
1.20	250.00	2000	826.0	27.319	1.2337	0.3893	725	0.00035	0.548	179.1	1.270	0.393	48.5
1.40	214.29	1942	803.9	27.324	1.2371	0.3835	711	0.00034	0.749	159.4	1.066	0.229	65.4
1.60	187.50	1893	787.3	27.327	1.2400	0.3790	699	0.00033	0.891	154.8	1.011	0.122	76.8
1.80	166.83	1851	771.4	27.329	1.2424	0.3753	689	0.00032	1.000	153.9	1.000	0.591	85.3
2.00	150.00	1813	757.2	27.331	1.2445	0.3722	679	0.00031	1.092	154.4	1.007	0.747	92.2
4.00	75.00	1578	671.9	27.337	1.2507	0.3504	617	0.00028	1.594	165.8	1.281	1.022	126.2
10.00	30.00	1303	576.1	27.339	1.2709	0.3411	539	0.00023	0.412	182.4	2.143	1.024	155.8
20.00	15.00	1142	515.1	27.339	1.2810	0.3309	484	0.00020	0.520	192.6	3.342	1.393	172.0
20.41	14.70	1117	512.5	27.339	1.2819	0.3308	482	0.00020	0.562	192.9	3.388	1.396	172.4
40.00	7.50	961	462.8	27.339	1.2929	0.3209	434	0.00018	2.947	201.2	5.330	1.496	184.7
100.00	3.00	777	405.0	27.339	1.3095	0.3076	367	0.00015	3.487	210.3	10.060	1.603	197.9
200.00	1.50	658	366.9	27.339	1.3227	0.2979	321	0.00012	3.919	215.8	16.399	1.666	205.7
400.00	.75	554	336.5	27.339	1.3364	0.2887	279	0.00011	4.380	220.3	26.792	1.717	212.0
1000.00	.30	438	305.5	27.339	1.3556	0.2782	229	0.00008	5.049	225.0	51.338	1.771	218.7
2000.00	.15	365	285.3	27.339	1.3753	0.2728	195	0.00007	5.613	227.8	83.976	1.803	222.6
4000.00	.08	303	266.6	27.339	1.3977	0.2693	164	0.00006	6.435	230.1	137.459	1.830	225.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb/in. ² abs	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)·cm	Mach number, M	Specific impulse in vacuum, I_{vac} , sec	Area ratio, ϵ	Thrust coefficient, C_T , lb(sec)/(lb)	Specific impulse, I , lb(sec)/(lb)
$R = 0.150$, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	600.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000	530.0	2.250	0.000	0.0
1.05	571.43	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	.271	527	2.297	.210	47.4
1.20	500.00	1129	5218.6	4.416	1.3436	1.7597	303	0.00070	.527	334.2	1.297	.403	90.8
1.40	428.57	1085	5141.8	4.416	1.3469	1.7472	293	0.00068	.722	296.1	1.081	.543	122.2
1.60	375.00	1049	5077.7	4.416	1.3497	1.7370	285	0.00066	.860	286.6	1.018	.636	143.2
1.87	321.68	1008	5006.8	4.416	1.3528	1.7256	276	0.00063	1.000	284.1	1.000	.725	163.4
2.00	300.00	989	4975.4	4.416	1.3551	1.7210	272	0.00062	1.059	284.4	1.003	.761	171.5
4.00	150.00	824	4693.4	4.416	1.3651	1.6824	234	0.00052	1.566	301.7	1.233	1.031	232.3
10.00	60.00	643	4392.5	4.416	1.3748	1.6506	188	0.00042	2.152	327.5	1.974	1.257	283.1
20.00	30.00	532	4209.8	4.416	1.3799	1.6345	159	0.00035	2.586	343.5	2.983	1.376	309.9
40.00	15.00	439	4058.9	4.416	1.3824	1.6269	133	0.00029	3.031	356.4	4.620	1.467	330.4
40.83	14.70	437	4054.8	4.416	1.3824	1.6267	132	0.00029	3.044	356.8	4.682	1.469	330.9
100.00	6.00	340	3899.0	4.416	1.3883	1.6089	104	0.00023	3.648	369.8	8.432	1.558	350.8
200.00	3.00	280	3802.6	4.416	1.3930	1.5951	85	0.00018	4.148	377.7	13.431	1.610	362.6
400.00	1.50	230	3723.2	4.416	1.4069	1.5598	70	0.00015	4.674	384.1	21.488	1.652	372.0
1000.00	.60	175	3640.1	4.416	1.4347	1.4852	55	0.00011	5.438	390.6	39.928	1.694	381.6
2000.00	.30	142	3590.9	4.416	1.4552	1.4387	45	0.00009	6.096	394.3	63.572	1.719	387.2
4000.00	.15	114	3551.2	4.416	1.4777	1.4039	36	0.00007	6.842	397.3	100.938	1.739	391.6
$R = 0.200$, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	600.00	1514	2969.7	5.216	1.3078	1.6187	402	0.00084	0.000	274	2.233	.209	49.3
1.05	571.43	1497	2941.7	5.216	1.3089	1.6143	399	0.00083	.274	552.1	1.289	.400	94.6
1.20	500.00	1450	2866.8	5.216	1.3119	1.6024	389	0.00081	.533	348.6	1.077	.537	127.4
1.40	428.57	1398	2783.1	5.216	1.3124	1.5888	378	0.00074	.730	309.3	1.000	.716	169.2
1.60	375.00	1354	2713.2	5.216	1.3185	1.5773	369	0.00076	.889	299.6	1.016	.632	149.4
1.85	324.94	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	297.3	1.000	.757	179.1
2.00	300.00	1282	2601.1	5.216	1.3236	1.5584	353	0.00072	1.068	297.8	1.004	.757	179.1
4.00	150.00	1079	2290.0	5.216	1.3391	1.5046	307	0.00061	1.572	316.7	1.244	1.029	243.2
10.00	60.00	452	1954.3	5.216	1.3558	1.4516	251	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	30.00	709	1748.8	5.216	1.3656	1.4232	213	0.00040	2.573	362.0	3.049	1.379	325.9
40.00	15.00	588	1578.0	5.216	1.3715	1.4066	179	0.00034	3.010	376.0	4.739	1.472	348.0
40.83	14.70	585	1573.4	5.216	1.3716	1.4062	178	0.00034	3.023	376.4	4.802	1.474	348.6
100.00	6.00	458	1396.3	5.216	1.3770	1.3916	142	0.00026	3.619	390.5	8.679	1.565	370.0
200.00	3.00	379	1286.1	5.216	1.3831	1.3808	117	0.00022	4.111	399.1	13.870	1.619	382.7
400.00	1.50	312	1195.2	5.216	1.3858	1.3684	96	0.00018	4.638	406.1	22.296	1.662	393.0
1000.00	.60	242	1098.9	5.216	1.3972	1.3402	74	0.00013	5.394	413.4	41.979	1.706	403.5
2000.00	.30	198	1041.1	5.216	1.4197	1.2976	61	0.00011	6.014	417.7	67.667	1.733	409.7
4000.00	.15	161	993.9	5.216	1.4562	1.2543	50	0.00009	6.701	421.1	108.754	1.754	414.6
$R = 0.250$, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	600.00	1817	1249.3	6.016	1.2827	1.4998	481	0.00092	0.000	563.4	2.218	0.000	0.0
1.05	571.43	1797	1220.2	6.016	1.2837	1.4955	477	0.00091	.276	552.1	1.283	.398	96.6
1.20	500.00	1745	1142.1	6.016	1.2865	1.4840	467	0.00089	.538	356.2	1.077	.536	130.1
1.40	428.57	1686	1054.7	6.016	1.2896	1.4712	456	0.00086	.736	316.3	1.015	.629	152.7
1.60	375.00	1636	981.5	6.016	1.2924	1.4604	446	0.00084	.876	308.6	1.000	.708	171.8
1.85	327.81	1587	909.9	6.016	1.2992	1.4494	436	0.00081	1.000	304.5	1.000	.754	183.1
2.00	300.00	1555	863.9	6.016	1.2971	1.4423	429	0.00080	1.076	305.1	1.005	.754	183.1
4.00	150.00	1322	535.1	6.016	1.3125	1.3874	378	0.00060	1.578	325.5	1.256	1.027	249.3
10.00	60.00	1057	176.1	6.016	1.3329	1.3225	314	0.00054	2.147	355.3	2.048	1.258	305.6
20.00	30.00	887	954.0	6.016	1.3440	1.2849	269	0.00046	2.563	373.7	3.127	1.382	335.7
40.00	15.00	741	9768.1	6.016	1.3568	1.2760	228	0.00036	2.987	388.7	4.883	1.478	359.0
40.83	14.70	737	9763.1	6.016	1.3571	1.2552	227	0.00038	3.000	389.1	4.949	1.481	359.6
100.00	6.00	581	9569.0	6.016	1.3663	1.2321	181	0.00030	3.581	404.2	8.985	1.575	382.4
200.00	3.00	482	9474.8	6.016	1.3717	1.2189	151	0.00025	4.064	413.4	14.396	1.630	395.9
400.00	1.50	399	9347.3	6.016	1.3755	1.2100	125	0.00020	4.582	420.9	23.208	1.675	406.8
1000.00	.60	310	9240.5	6.016	1.3820	1.1949	95	0.00015	5.327	428.7	43.893	1.722	418.1
2000.00	.30	256	9175.9	6.016	1.3883	1.1810	78	0.00012	5.945	433.4	71.279	1.749	424.7
4000.00	.15	210	9122.7	6.016	1.4037	1.1485	64	0.00010	6.606	437.2	115.650	1.771	430.2
$R = 0.300$, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	600.00	2094	9932.7	6.815	1.2613	1.4145	551	0.00098	0.000	568.6	2.206	.206	50.8
1.05	571.43	2073	9903.1	6.815	1.2623	1.4097	547	0.00097	.279	559.8	2.277	.396	97.5
1.20	500.00	2016	9823.5	6.815	1.2620	1.3967	537	0.00095	.542	359.8	1.071	.553	131.4
1.40	428.57	1952	9734.3	6.815	1.2661	1.3825	525	0.00092	.742	319.8	1.015	.620	154.2
1.60	375.00	1898	9659.4	6.816	1.2708	1.3706	515	0.00089	.882	310.3	1.013	.620	154.2
1.82	330.21	1847	9589.9	6.816	1.2734	1.3598	505	0.00087	1.000	308.3	1.000	.701	174.7
2.00	300.00	1809	9538.8	6.816	1.2753	1.3519	498	0.00085	1.082	309.1	1.006	.751	185.1
4.00	150.00	1553	9199.6	6.816	1.2894	1.2991	445	0.00074	1.585	330.6	1.266	1.025	252.6
10.00	60.00	1257	8825.3	6.816	1.3095	1.2336	375	0.00060	2.148	361.8	2.085	1.260	310.4
20.00	30.00	1064	8591.1	6.816	1.3248	1.1891	325	0.00051	2.555	381.2	3.206	1.386	341.7
40.00	14.70	891	8380.2	6.816	1.3288	1.1522	277	0.00042	2.981	397.4	5.106	1.488	366.6
40.83	15.00	895	8393.6	6.816	1.3384	1.1531	279	0.00042	2.988	397.0	5.037	1.485	366.0
100.00	6.00	707	8180.3	6.816	1.3520	1.1174	223	0.00033	3.544	413.5	9.324	1.585	390.5
200.00	3.00	590	8049.6	6.816	1.3603	1.1007	187	0.00027	4.013	423.3	14.993	1.643	404.8</td

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb./sq.in abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isoenthalpic exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/sec·°K/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , sec	Area ratio, E	Thrust coefficient, C _F	Specific impulse, I, lb.sec/lb
R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	600.00	2347	8892.8	7.610	1.2410	1.3691	611	0.00104	0.000			0.000	0.0
1.05	571.43	2325	8863.0	7.610	1.2421	1.3521	608	0.00103	.281	570.0	2.195	.205	50.4
1.20	500.00	2266	8783.0	7.611	1.2451	1.3440	598	0.00100	.264	361.0	1.273	.194	51.7
1.40	428.57	2198	8693.2	7.613	1.2485	1.3249	586	0.00097	.247	321.2	1.068	.151	191.8
1.60	375.00	2140	8617.6	7.613	1.2513	1.3099	576	0.00094	.187	311.8	1.012	.023	154.7
1.81	332.36	2089	8551.1	7.613	1.2538	1.2974	567	0.00092	1.000	310.0	1.000	.095	172.5
2.00	300.00	2046	8495.7	7.613	1.2559	1.2874	559	0.00090	1.088	310.9	1.000	.074	185.9
4.00	150.00	1771	8150.9	7.616	1.2699	1.2291	506	0.00079	1.950	333.2	1.275	1.023	256.1
10.00	60.00	1451	7766.6	7.616	1.2885	1.1655	434	0.00065	2.149	365.6	2.119	1.261	313.0
20.00	30.00	1238	7523.9	7.616	1.3036	1.1204	381	0.00055	2.550	385.8	3.281	1.390	349.1
40.83	14.70	1045	7311.7	7.616	1.3192	1.0783	328	0.00046	2.965	402.9	5.260	1.494	370.9
40.00	15.00	1050	7317.3	7.616	1.3188	1.0794	330	0.00046	2.953	402.5	5.188	1.491	370.3
100.00	6.00	838	7092.4	7.616	1.3364	1.0365	267	0.00036	3.511	419.8	9.676	1.594	395.8
200.00	3.00	702	6953.5	7.616	1.3475	1.0118	225	0.00030	3.564	430.2	15.066	1.674	416.8
400.00	1.50	586	6837.3	7.616	1.3593	.9953	188	0.00025	4.453	438.6	25.350	1.703	432.9
1000.00	.60	460	6712.8	7.616	1.3634	.9789	148	0.00019	5.162	447.0	48.288	1.754	439.5
2000.00	.30	382	6636.9	7.616	1.3684	.9692	121	0.00016	5.751	452.8	78.852	1.784	443.1
4000.00	.15	317	6573.8	7.616	1.3738	.9590	98	0.00013	6.392	457.2	128.949	1.809	449.2
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	600.00	2574	8050.5	8.436	1.2209	1.3697	663	0.00110	0.000			0.000	0.0
1.05	571.43	2552	8020.9	8.437	1.2220	1.3599	660	0.00109	.283	568.5	2.184	.204	50.7
1.20	500.00	2492	7941.2	8.401	1.2252	1.3344	650	0.00106	.550	360.5	1.268	.392	7.5
1.40	428.57	2422	7851.7	8.404	1.2289	1.3072	639	0.00102	.752	321.0	1.065	.526	194.9
1.60	375.00	2363	7776.1	8.406	1.2320	1.2896	630	0.00100	.895	311.8	1.011	.621	154.5
1.79	334.53	2313	7713.0	8.408	1.2347	1.2685	621	0.00097	1.000	310.2	1.000	.668	171.4
2.00	300.00	2266	7654.1	8.410	1.2372	1.2533	613	0.00095	1.094	311.2	1.008	.746	185.7
4.00	150.00	1978	7306.9	8.414	1.2520	1.1787	561	0.00083	1.594	334.3	1.284	1.022	254.4
10.00	60.00	1637	6916.6	8.416	1.2701	1.1109	489	0.00069	2.149	367.6	2.150	1.262	314.1
20.00	30.00	1408	6667.8	8.416	1.2842	1.0669	434	0.00059	2.545	388.6	3.351	1.393	366.9
40.83	14.70	1199	6448.5	8.416	1.2996	1.0242	379	0.00050	2.951	406.3	5.409	1.500	373.4
100.00	6.00	970	6219.6	8.416	1.3188	.9767	313	0.00040	3.482	424.1	10.429	1.603	399.1
200.00	3.00	818	6073.7	8.416	1.3318	.9478	266	0.00033	3.920	435.0	16.282	1.666	414.7
400.00	1.50	687	5950.8	8.416	1.3428	.9249	224	0.00027	4.391	443.9	26.525	1.717	427.4
1000.00	.60	542	5818.5	8.416	1.3537	.9037	176	0.00021	5.076	453.3	50.761	1.770	440.7
2000.00	.30	452	5737.3	8.416	1.3595	.8928	146	0.00017	5.648	459.0	83.105	1.802	448.6
4000.00	.15	376	5669.7	8.416	1.3647	.8835	119	0.00014	6.271	463.6	136.261	1.828	455.1
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	600.00	2773	7354.5	9.167	1.2018	1.4156	707	0.00119	0.000			0.000	0.0
1.05	571.43	2752	7325.3	9.170	1.2029	1.4027	704	0.00118	.285	565.0	2.172	.203	50.4
1.20	500.00	2692	7246.5	9.177	1.2060	1.3686	695	0.00114	.554	358.6	1.263	.390	96.9
1.40	428.57	2622	7157.9	9.184	1.2097	1.3318	685	0.00110	.757	319.6	1.063	.526	130.8
1.60	375.00	2566	7082.9	9.189	1.2128	1.3022	676	0.00106	.899	310.7	1.010	.618	153.7
1.78	336.72	2517	7023.8	9.193	1.2154	1.2799	669	0.00104	1.000	309.2	1.000	.662	169.6
2.00	300.00	2467	6961.6	9.197	1.2183	1.2573	661	0.00101	1.100	310.3	1.009	.743	184.9
4.00	150.00	2174	6614.5	9.210	1.2347	1.1514	611	0.00087	1.599	334.2	1.293	1.020	253.7
10.00	60.00	1817	6220.9	9.215	1.2537	1.0682	540	0.00072	2.149	368.3	2.182	1.283	314.1
20.00	30.00	1575	5967.7	9.216	1.2670	1.0237	485	0.00063	2.539	389.9	3.620	1.397	367.4
40.83	14.70	1357	5749.0	9.216	1.2811	.9828	429	0.00054	2.927	407.8	5.476	1.503	373.8
100.00	6.00	1104	5506.6	9.216	1.3008	.9325	358	0.00043	3.455	426.8	10.381	1.612	401.0
200.00	3.00	927	5354.4	9.216	1.3132	.8996	307	0.00036	3.879	438.3	16.950	1.678	417.2
400.00	1.50	792	5225.4	9.216	1.3282	.8727	281	0.00030	4.334	447.7	27.755	1.731	430.4
1000.00	.60	629	5085.6	9.216	1.3418	.8465	207	0.00023	4.994	457.6	53.398	1.787	444.9
2000.00	.30	526	4999.5	9.216	1.3502	.8313	172	0.00019	5.584	463.6	87.14	1.820	452.7
4000.00	.15	439	4927.5	9.216	1.3562	.8210	142	0.00016	6.148	468.5	144.197	1.848	459.5
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	600.00	2944	6769.6	9.919	1.1849	1.5012	745	0.00130	0.000			0.000	0.0
1.05	571.43	2923	6741.0	9.923	1.1859	1.4856	742	0.00129	.287	559.8	2.162	.202	50.0
1.20	500.00	2866	6663.6	9.935	1.1835	1.4440	734	0.00124	.558	355.7	1.258	.388	76.1
1.40	428.57	2800	6576.3	9.947	1.1917	1.3979	724	0.00119	.762	317.3	1.061	.524	129.7
1.60	375.00	2742	6502.4	9.957	1.1946	1.3600	716	0.00115	.904	308.6	1.009	.616	152.5
1.77	338.88	2699	6447.5	9.963	1.1970	1.3324	710	0.00112	1.000	307.3	1.000	.676	167.4
2.00	300.00	2647	6382.5	9.971	1.1998	1.3008	702	0.00109	1.106	308.6	1.010	.741	185.9
4.00	150.00	2356	6037.6	9.999	1.2169	1.1551	655	0.00092	1.603	333.1	1.303	1.019	252.4
10.00	60.00	1990	5642.7	10.013	1.2378	1.0408	587	0.00076	2.147	368.0	2.216	1.264	313.1
20.00	30.00	1737	5386.6	10.015	1.2515	.9888	532	0.00066	2.532	390.1	3.491	1.401	346.9
40.83	14.70	1507	5163.7	10.016	1.2647	.9482	477	0.00057	2.914	408.6	5.620	1.509	373.8
100.00	6.00	1238	4914.9	10.016	1.2834	.9884	403	0.00046	3.431	428.3	10.736	1.622	401.7
200.00	3.00	1059	4757.3	10.016	1.2984	.8634	350	0.00039	3.842	440.3	17.634	1.690	418.5
400.00	1.50	900	4622.8	10.016	1.3125	.8333	300	0.00032	4.280	450.2	29.032	1.745	432.2
1000.00	.60	720	4476.0	10.016	1.3291	.8013	240	0.00025	4.914	460.7	56.203	1.804	446.7
2000.00	.30	606	4385.0	10.016	1.3387	.7841	201	0.00021	5.445	461.0	92.675	1.839	455.5
4000.00	.15	507	4308.7	10.016	1.3473	.7696	166	0.00017	6.024	472.2	152.844	1.868	462.7

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN
 [Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute,
 equilibrium composition during isentropic expansion

Pressure ratio, P _c /P _a	Static pressure, P _a , lb/sq in abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isoentropic exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec·°K cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , sec	Area ratio, ε	Thrust coefficient, C _T	Specific impulse, I, (lb/sec)/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	600.00	3208	5841.6	11.347	1.1593	1.7671	803	0.00150	0.000	546.7	2.144	0.000	0.0
1.05	571.43	3189	5814.3	11.356	1.1598	1.7482	801	0.00158	0.291	534.7	2.000	.48.8	
1.20	500.00	3137	5740.5	11.379	1.1611	1.6966	794	0.00172	.564	347.0	1.250	.385	93.8
1.40	428.57	3077	5656.9	11.404	1.1629	1.6375	786	0.00146	.770	310.0	1.057	.520	126.8
1.60	375.00	3025	5586.0	11.425	1.1646	1.5869	779	0.00140	.913	302.6	1.007	.612	149.1
1.75	342.61	2990	5538.0	11.438	1.1659	1.5531	771	0.00137	1.000	301.5	1.000	.666	162.3
2.00	300.00	2938	5470.4	11.457	1.1680	1.5041	766	0.00132	1.117	303.1	1.012	.737	179.7
4.00	150.00	2669	5134.6	11.535	1.1817	1.2723	727	0.00108	1.613	328.7	1.323	1.017	248.0
10.00	60.00	2313	4742.5	11.593	1.2048	1.0538	667	0.00085	2.145	365.0	2.288	1.268	309.3
20.00	30.00	2050	4483.6	11.609	1.2216	0.9574	617	0.00072	2.517	388.2	3.644	1.410	343.7
40.00	15.00	1803	4255.3	11.615	1.2359	0.896	564	0.00063	2.855	407.6	5.926	1.524	371.5
40.83	14.70	1796	4249.0	11.615	1.2363	0.893	562	0.00053	2.896	408.2	6.013	1.527	372.3
100.00	6.00	1506	3996.4	11.616	1.2528	0.8482	490	0.00052	3.381	428.7	11.474	1.643	400.7
200.00	3.00	1306	3829.9	11.616	1.2663	0.8136	434	0.00045	3.772	441.6	19.054	1.716	418.4
400.00	1.50	1125	3686.0	11.616	1.2806	0.7807	379	0.00038	4.182	452.4	31.724	1.776	433.1
1000.00	.60	916	3526.4	11.616	1.2996	0.7420	311	0.00030	4.769	464.0	62.274	1.841	448.8
2000.00	.30	778	3426.2	11.616	1.3130	0.7177	264	0.00025	5.257	471.1	103.640	1.880	458.4
4000.00	.15	658	3341.2	11.616	1.3245	0.6983	222	0.00020	5.791	476.9	172.288	1.913	466.4
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	600.00	3381	5138.3	12.664	1.1429	2.1301	846	0.00177	0.000	531.5	2.133	0.000	0.0
1.05	571.43	3364	5112.5	12.677	1.1430	2.1115	843	0.00175	.293	531.5	2.133	.199	47.6
1.20	500.00	3317	5042.7	12.711	1.1433	2.0594	837	0.00189	.568	338.5	1.245	.383	91.2
1.40	428.57	3263	4963.5	12.750	1.1438	1.9976	830	0.00182	.775	302.7	1.054	.517	123.3
1.60	375.00	3217	4896.2	12.782	1.1443	1.9428	823	0.00176	.920	295.1	1.006	.609	145.2
1.75	345.24	3188	4855.0	12.802	1.1447	1.9085	819	0.00172	1.000	294.1	1.000	.659	157.0
2.00	300.00	3140	4786.1	12.834	1.1456	1.8496	813	0.00166	1.125	295.9	1.014	.734	175.1
4.00	150.00	2903	4463.7	12.978	1.1526	1.5556	779	0.00136	1.623	322.1	1.339	1.016	242.3
10.00	60.00	2584	4080.8	13.115	1.1702	1.2090	730	0.00102	2.148	359.5	2.356	1.273	303.3
20.00	30.00	2337	3823.0	13.174	1.1864	1.0195	688	0.00043	2.506	383.6	3.803	1.419	338.3
40.00	15.00	2088	3592.0	13.203	1.2067	0.9006	640	0.00070	3.455	404.1	6.256	1.539	366.8
40.83	14.70	2081	3585.6	13.203	1.2072	0.8980	638	0.00049	2.866	404.6	6.350	1.542	367.6
100.00	6.00	1775	3326.0	13.214	1.2263	.8183	571	0.0007	3.327	426.4	12.271	1.666	397.1
200.00	3.00	1558	3152.5	13.216	1.2387	0.7809	515	0.00040	3.700	440.2	20.571	1.744	415.7
400.00	1.50	1359	3000.6	13.216	1.2515	0.7484	459	0.00034	4.089	451.9	34.597	1.809	431.3
1000.00	.60	1125	2829.9	13.216	1.2696	0.7080	387	0.00035	4.637	464.6	68.879	1.880	448.2
2000.00	.30	968	2721.0	13.216	1.2840	0.6798	334	0.00029	5.087	472.4	115.835	1.924	458.6
4000.00	.15	820	2627.5	13.216	1.2978	0.6552	286	0.00024	5.575	479.0	194.445	1.961	467.4
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	600.00	3481	4586.0	13.859	1.1337	2.4909	875	0.00214	0.000	515.6	2.126	.198	44.0
1.05	571.43	3465	4562.6	13.875	1.1335	2.4777	873	0.00212	.294	515.6	2.126	.198	44.0
1.20	500.00	3422	4496.5	13.919	1.1331	2.4401	867	0.00217	.570	328.6	1.242	.381	88.5
1.40	428.57	3373	4422.2	13.969	1.1327	2.3938	861	0.00211	.778	294.1	1.052	.516	119.7
1.60	375.00	3331	4358.0	14.012	1.1324	2.3513	855	0.00216	.928	286.7	1.006	.607	140.9
1.75	346.81	3306	4321.9	14.037	1.1323	2.3254	851	0.00213	1.000	286.0	1.000	.656	151.8
2.00	300.00	3263	4254.0	14.082	1.1321	2.2752	845	0.00207	1.129	287.8	1.015	.733	170.0
4.00	150.00	3052	3948.2	14.288	1.1330	2.0021	816	0.00177	1.630	314.1	1.350	1.016	235.7
10.00	60.00	2779	3579.7	14.522	1.1403	1.5823	775	0.00116	2.155	351.9	2.409	1.276	296.0
20.00	30.00	2568	3327.2	14.656	1.1527	1.2725	741	0.00117	2.505	376.8	3.944	1.427	331.1
40.00	15.00	2346	3097.0	14.745	1.1712	1.0267	703	0.00044	2.837	398.3	6.587	1.552	360.1
40.83	14.70	2340	3090.5	14.747	1.1718	1.0207	702	0.00043	2.846	398.8	6.689	1.555	360.8
100.00	6.00	2042	2826.6	14.800	1.1976	.8369	642	0.0005	3.275	421.8	13.134	1.687	391.4
200.00	3.00	1815	2667.3	14.812	1.2135	0.7683	593	0.00045	3.623	436.6	22.231	1.771	410.8
400.00	1.50	1602	2488.5	14.815	1.2260	0.7287	557	0.00048	3.991	449.2	37.727	1.842	427.3
1000.00	.60	1347	2307.6	14.816	1.2422	.6880	464	0.00040	4.507	463.0	76.063	1.919	445.3
2000.00	.30	1173	2190.6	14.816	1.2553	0.6594	409	0.00034	4.926	471.6	129.237	1.968	456.6
4000.00	.15	1016	2089.0	14.816	1.2694	0.6320	356	0.00028	5.375	478.9	219.200	2.009	466.2
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	600.00	3526	4142.9	14.930	1.1295	2.6696	896	0.00214	0.000	500.1	2.123	0.000	0.0
1.05	571.43	3511	4120.1	14.948	1.1293	2.6628	894	0.00213	.294	500.1	2.123	.198	44.6
1.20	500.00	3469	4058.3	14.999	1.1285	2.6632	888	0.00219	.571	318.8	1.241	.381	85.8
1.40	428.57	3424	3988.0	15.057	1.1277	2.6185	881	0.00215	.780	285.4	1.052	.515	116.1
1.60	375.00	3382	3928.2	15.107	1.1270	2.5953	876	0.00212	.926	278.3	1.005	.607	136.7
1.75	347.52	3360	3894.5	15.130	1.1267	2.5813	873	0.00209	1.000	277.6	1.000	.653	147.0
2.00	300.00	3317	3830.1	15.190	1.1260	2.5526	866	0.00215	1.132	279.4	1.016	.732	165.0
4.00	150.00	3122	3540.7	15.441	1.1256	2.3886	839	0.00214	1.633	305.3	1.350	1.016	228.9
10.00	60.00	2881	3190.4	15.751	1.1229	2.0940	803	0.00141	2.161	342.8	2.437	1.278	287.9
20.00	30.00	2705	2947.8	15.963	1.1254	1.8100	775	0.00132	2.512	367.9	4.032	1.431	322.5
40.00	15.00	2520	2723.3	16.145	1.1327	1.4813	746	0.00122	2.838	390.0	6.838	1.560	351.5
40.83	14.70	2523	2716.9	16.150	1.1330	1.4712	745	0.00121	2.848	390.6	6.947	1.563	352.3
100.00	6.00	2279	2453.5	16.318	1.1553	1.0541	701	0.0005	3.246	414.9	13.977	1.702	383.4
200.00	3.00	2072	2270.2	16.384	1.1797	.8410	659	0.00055	3.555	430.8	24.037	1.791	403.7
400.00	1												

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P _s , lb/sq.in obs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscosity, μ, micro poise	Thermal conductivity, k, cal/(sec·°K)cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb/sec)/lb	Area ratio, ε	Thrust coefficient, C _f	Specific impulse, I, (lb·sec)/lb
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	600.00	3534	3777.9	15.886	1.1283	2.6093	910	0.00251	0.000	485.3	2.122	0.000	0.0
1.05	571.43	3519	3756.4	15.906	1.1280	2.6007	907	0.00250	0.295	485.3	1.198	43.3	
1.20	500.00	3478	3698.1	15.961	1.1272	2.5874	902	0.00247	0.572	309.4	1.240	0.381	83.3
1.40	428.57	3431	3631.9	16.024	1.1263	2.5703	895	0.00244	0.780	277.0	1.051	0.515	112.7
1.60	375.00	3392	3575.5	16.078	1.1255	2.5542	889	0.00241	0.926	270.2	1.005	0.606	132.7
1.73	347.72	3370	3544.0	16.108	1.1251	2.5445	886	0.00239	1.000	269.4	1.000	0.652	142.7
2.00	300.00	3327	3483.1	16.168	1.1244	2.5243	880	0.00236	1.132	271.3	1.016	0.732	160.1
4.00	150.00	3137	3210.2	16.441	1.1212	2.4094	852	0.00218	1.634	496.5	1.357	1.016	222.3
10.00	60.00	2903	2879.3	16.785	1.1186	2.2079	817	0.00192	2.162	333.1	2.445	1.270	279.6
20.00	30.00	2738	2649.6	17.030	1.1181	2.0216	791	0.00171	2.514	357.7	4.055	1.432	313.3
40.00	15.00	2578	2436.1	17.258	1.1191	1.8120	765	0.00150	2.842	379.5	6.910	1.562	341.7
40.83	14.70	2573	2430.0	17.265	1.1191	1.8056	764	0.00149	2.852	380.1	7.022	1.565	342.5
100.00	6.00	2371	2177.0	17.526	1.1239	1.5117	728	0.00120	3.255	404.6	14.326	1.706	373.2
200.00	3.00	2214	1997.7	17.695	1.1315	1.2810	697	0.00099	3.558	421.1	25.124	1.799	393.6
400.00	1.50	2052	1832.3	17.830	1.1437	1.0654	663	0.00080	3.857	435.6	44.210	1.881	411.4
1000.00	.60	1826	1634.9	17.947	1.1679	.8338	611	0.00059	4.260	452.2	93.124	1.974	431.8
2000.00	.30	1648	1501.7	17.991	1.1894	.7163	564	0.00048	4.365	462.6	162.695	2.034	445.0
4000.00	.15	1470	1382.4	18.009	1.2091	.6444	514	0.00040	4.942	472.0	282.648	2.087	456.5
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	600.00	3374	2626.1	19.463	1.1327	1.6233	930	0.00163	0.000	0.000	0.000	0.000	0.0
1.20	500.00	3315	2563.9	19.540	1.1321	1.5942	921	0.00158	.571	273.0	1.242	0.381	73.5
1.40	571.43	3356	2609.3	19.483	1.1325	1.6157	927	0.00162	.294	428.4	2.125	1.198	38.2
1.60	428.57	3267	2512.4	19.604	1.1317	1.5682	913	0.00155	.779	244.3	1.052	0.516	99.4
1.73	375.00	3226	2466.5	19.658	1.1314	1.5447	906	0.00151	.924	238.3	1.006	0.607	117.1
2.00	300.00	3158	2396.7	19.748	1.1310	1.5034	896	0.00146	1.130	237.6	1.000	0.654	126.1
4.00	150.00	2953	2185.1	20.011	1.1313	1.3606	862	0.00128	1.631	261.0	1.351	1.016	195.9
10.00	60.00	2692	1930.2	20.314	1.1356	1.474	818	0.00105	2.157	292.6	2.415	1.276	246.1
20.00	30.00	2496	1755.2	20.499	1.1432	.9816	782	0.00086	2.209	313.5	3.967	1.428	275.3
40.00	15.00	2297	1594.7	20.640	1.1557	.8274	743	0.00070	2.841	331.7	6.664	1.554	299.6
40.83	14.70	2291	1590.2	20.643	1.1562	.8232	742	0.00070	2.850	332.2	6.768	1.557	300.2
100.00	6.00	2026	1404.5	20.752	1.1791	.6682	685	0.00054	3.268	351.9	13.428	1.691	326.0
200.00	3.00	1818	1277.1	20.792	1.1984	.5904	635	0.00045	3.599	364.7	22.891	1.777	342.6
400.00	1.50	1616	1163.4	20.807	1.2152	.5532	582	0.00039	3.950	375.6	39.039	1.850	356.7
1000.00	.60	1366	1033.2	20.812	1.2336	.5048	509	0.00032	4.450	387.5	79.054	1.931	372.3
2000.00	.30	1195	948.5	20.813	1.2462	.4834	454	0.00027	4.858	395.0	134.733	1.982	382.1
4000.00	.15	1039	874.7	20.813	1.2594	.4636	401	0.00023	5.296	401.4	229.310	2.025	390.4
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	600.00	3158	2016.0	21.832	1.1414	1.1081	919	0.00112	0.000	0.000	0.000	0.000	0.0
1.05	571.43	3141	2002.0	21.850	1.1414	1.1005	917	0.00111	.293	391.2	2.132	1.199	34.9
1.20	500.00	3097	1964.2	21.900	1.1417	1.0794	909	0.00108	.568	249.2	1.245	0.383	67.1
1.40	428.57	3048	1921.3	21.956	1.1421	1.0543	900	0.00105	.776	222.9	1.054	0.517	90.8
1.60	375.00	3002	1884.8	22.003	1.1426	1.0320	893	0.00102	.920	217.2	1.006	0.609	106.9
1.73	345.45	2975	1862.7	22.031	1.1430	1.0182	888	0.00100	1.000	216.6	1.000	0.658	115.5
2.00	300.00	2929	1825.1	22.078	1.1437	.9940	880	0.00097	1.125	217.9	1.014	.734	128.9
4.00	150.00	2708	1650.0	22.286	1.1496	.8720	840	0.00083	1.624	237.3	1.341	1.016	178.4
10.00	60.00	2413	1442.0	22.490	1.1641	.7166	784	0.00065	2.151	265.0	2.365	1.273	223.5
20.00	30.00	2189	1301.4	22.588	1.1804	.6182	737	0.00054	2.507	283.0	3.829	1.421	249.4
40.00	15.00	1965	1174.9	22.642	1.1988	.5549	686	0.00045	2.852	298.3	6.321	1.541	270.5
40.83	14.70	1959	1171.4	22.643	1.1994	.5541	684	0.00045	2.863	298.7	6.416	1.544	271.1
100.00	6.00	1678	1028.7	22.670	1.2212	.4875	614	0.00037	3.316	514.9	12.437	1.670	293.1
200.00	3.00	1475	932.9	22.676	1.2351	.4613	557	0.00032	3.683	525.3	20.879	1.749	307.0
400.00	1.50	1289	849.1	22.677	1.2476	.4417	501	0.00028	4.069	334.1	35.155	1.815	318.7
1000.00	.60	1070	754.5	22.677	1.2641	.4194	430	0.00023	4.614	343.6	70.143	1.887	331.3
2000.00	.30	923	694.1	22.677	1.2770	.4040	378	0.00019	5.059	349.5	118.235	1.932	339.2
4000.00	.15	792	642.1	22.677	1.2904	.3894	329	0.00016	5.539	354.5	199.011	1.970	345.8
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	600.00	2747	1381.4	24.718	1.1694	0.6509	869	0.00065	0.000	0.000	0.000	0.000	0.0
1.05	571.43	2729	1370.7	24.729	1.1701	.6451	866	0.00065	.289	342.7	2.152	.201	30.6
1.20	500.00	2679	1341.7	24.759	1.1723	.6293	856	0.00062	.561	217.9	1.254	.386	58.8
1.40	428.57	2622	1308.9	24.790	1.1749	.6114	845	0.00060	.766	194.6	1.058	.522	79.4
1.60	375.00	2573	1281.4	24.815	1.1774	.5963	835	0.00058	.909	189.4	1.008	.613	93.4
1.73	340.99	2538	1261.7	24.832	1.1793	.5888	828	0.00057	1.000	188.6	1.000	.670	102.1
2.00	300.00	2491	1235.9	24.852	1.1819	.5720	819	0.00055	1.112	189.5	1.011	.739	112.5
4.00	150.00	2237	1105.1	24.937	1.1983	.5059	765	0.00046	1.608	205.1	1.314	1.018	155.0
10.00	60.00	1913	953.9	24.990	1.2209	.4460	690	0.00038	2.146	227.2	2.253	1.266	192.9
20.00	30.00	1682	854.9	25.003	1.2359	.4185	631	0.00033	2.524	241.2	3.569	1.405	214.0
40.00	15.00	1470	768.2	25.007	1.2483	.4000	572	0.00029	2.900	253.0	5.778	1.517	231.0
40.83	14.70	1464	765.8	25.007	1.2487	.3995	571	0.00028	2.911	253.3	5.862	1.520	231.4
100.00	6.00	1220	670.5	25.008	1.2535	.3811	498	0.00024	3.408	265.7	11.130	1.633	248.7
200.00	3.00	1053	608.0	25.008	1.2755	.3679	444	0.00021	3.807	273.4	18.422	1.703	259.4
400.00	1.50	904	554.2	25.008	1.2879	.3555	392	0.00018	4.229	279.9	30.593	1.761	268.3
1000.00</td													

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P _s in abs., lb/in. ²	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c _p , cal/(g°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb-sec)/lb	Area ratio, ε	Thrust coefficient, C _f	Specific impulse, I, (lb-sec)/lb
$R = 4.000, \text{ PERCENT FUEL} = 3.054, \text{ O/F} = 31.746$													
1.00	600.00	2381	1054.4	26.323	1.2036	0.4697	806	0.00045	0.000			0.000	0.0
1.05	571.43	2362	1045.7	26.328	1.2048	0.4663	802	0.00045	.285	308.9	2.174	.203	27.6
1.20	500.00	2309	1022.1	26.340	1.2079	0.4572	790	0.00044	.554	196.0	1.263	.390	53.0
1.40	428.57	2249	995.6	26.352	1.2116	0.4473	777	0.00042	.756	174.7	1.063	.526	71.5
1.60	375.00	2198	973.2	26.361	1.2149	0.4393	765	0.00041	.898	169.8	1.010	.618	84.0
1.78	336.49	2157	955.5	26.367	1.2175	0.4332	756	0.00040	1.000	169.0	1.000	.683	92.8
2.00	300.00	2113	937.0	26.374	1.2202	0.4272	746	0.00039	1.099	169.6	1.009	.744	101.1
4.00	150.00	1860	833.4	26.396	1.2355	0.3982	685	0.00034	1.599	182.6	1.293	1.020	138.7
10.00	60.00	1554	715.9	26.405	1.2521	0.3763	602	0.00028	2.182	401.3	2.182	1.263	171.6
20.00	30.00	1348	640.3	26.406	1.2632	0.3612	546	0.00025	2.542	213.1	3.423	1.397	189.8
40.00	15.00	1164	574.8	26.408	1.2741	0.3499	491	0.00022	2.931	222.9	5.493	1.503	204.3
40.83	14.70	1159	573.1	26.406	1.2744	0.3495	489	0.00022	2.943	223.2	5.572	1.506	204.7
100.00	6.00	952	502.1	26.406	1.2895	0.3352	421	0.00018	3.458	233.4	10.461	1.613	219.2
200.00	3.00	813	456.1	26.406	1.3022	0.3243	371	0.00016	3.876	239.8	17.162	1.679	228.2
400.00	1.50	690	417.0	26.406	1.3153	0.3139	325	0.00013	4.320	245.1	28.237	1.733	235.5
1000.00	.60	551	374.4	26.406	1.3331	0.3012	269	0.00011	4.959	250.7	54.608	1.790	243.3
2000.00	.30	463	348.0	26.406	1.3460	0.2927	232	0.00009	5.492	254.0	89.893	1.824	247.9
4000.00	.15	386	325.9	26.406	1.3564	0.2864	197	0.00007	6.079	256.8	147.835	1.853	251.8
$R = 5.000, \text{ PERCENT FUEL} = 2.458, \text{ O/F} = 39.683$													
1.00	600.00	2072	855.0	27.317	1.2317	0.3924	742	0.00036	0.000			0.000	0.0
1.05	571.43	2053	847.7	27.319	1.2327	0.3906	738	0.00036	.282	482.7	2.190	.204	25.2
1.20	500.00	2002	828.0	27.323	1.2355	0.3859	725	0.00035	.548	179.1	1.270	.393	48.5
1.40	428.57	1944	805.9	27.326	1.2387	0.3808	711	0.00034	.749	159.4	1.067	.530	65.4
1.60	375.00	1894	787.2	27.329	1.2413	0.3767	699	0.00033	.890	154.8	1.011	.622	76.8
1.80	333.54	1852	771.3	27.331	1.2436	0.3734	689	0.00032	1.000	154.0	1.000	.691	85.3
2.00	300.00	1813	757.2	27.332	1.2455	0.3706	679	0.00031	1.092	154.4	1.007	.747	92.3
4.00	150.00	1578	671.8	27.337	1.2571	0.3559	617	0.00028	1.594	165.8	1.281	1.023	126.2
10.00	60.00	1303	576.1	27.339	1.2710	0.3410	559	0.00023	2.152	182.2	2.143	1.262	155.8
20.00	30.00	1122	515.1	27.339	1.2815	0.3309	484	0.00020	2.551	192.6	3.341	1.393	172.0
40.00	15.00	961	462.7	27.339	1.2929	0.3209	432	0.00018	2.948	201.2	5.329	1.497	184.7
40.83	14.70	956	461.3	27.339	1.2932	0.3206	430	0.00018	2.959	201.4	5.405	1.499	185.1
100.00	6.00	777	405.0	27.339	1.3095	0.3076	367	0.00015	3.488	210.3	10.063	1.603	197.9
200.00	3.00	658	368.9	27.339	1.3228	0.2979	321	0.00012	3.919	215.8	16.396	1.666	205.7
400.00	1.50	554	338.4	27.339	1.3364	0.2887	279	0.00011	4.380	220.3	26.787	1.717	214.0
1000.00	.60	438	305.5	27.339	1.3536	0.2782	229	0.00008	5.049	225.0	51.327	1.771	218.7
2000.00	.30	365	285.3	27.339	1.3633	0.2728	195	0.00007	5.614	227.8	83.959	1.803	222.6
4000.00	.15	303	268.6	27.339	1.3697	0.2693	164	0.00006	5.236	230.1	137.411	1.830	225.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Combustion-chamber pressure, 60 pounds per square inch absolute, frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb/sq.in. abs	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(g°C)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec°C)cm	Mach number, M	Specific impulse in vacuum, I_{vac} , sec	Area ratio, E	Thrust coefficient, C_f	Specific impulse, I , lb/(sec)/lb
$R = 0.150$, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	60.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000	2.250	.210	47.4	
1.05	57.14	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	.271	530.0	1.297	.403	90.8
1.20	50.00	1129	5218.5	4.416	1.3436	1.7597	303	0.00070	.527	334.2	1.000	.543	122.2
1.40	42.86	1085	5141.8	4.416	1.3469	1.7472	253	0.00068	.722	296.1	1.081	.543	122.2
1.60	37.50	1049	5077.7	4.416	1.3497	1.7369	285	0.00066	.860	286.6	1.018	.636	143.2
1.87	32.17	1008	5006.8	4.416	1.3528	1.7257	276	0.00063	1.000	284.1	1.000	.725	163.4
2.00	30.00	989	4975.4	4.416	1.3540	1.7210	272	0.00062	1.059	284.4	1.003	.761	171.5
4.00	15.00	824	4693.4	4.416	1.3651	1.6825	234	0.00052	1.566	301.7	1.233	1.031	244.3
4.08	14.70	819	4685.8	4.416	1.3654	1.6815	232	0.00052	1.579	304.3	1.244	1.036	233.7
10.00	6.00	643	4392.5	4.416	1.3748	1.6505	188	0.00042	2.152	327.5	1.974	1.257	281.1
20.00	3.00	532	4209.8	4.416	1.3799	1.6344	159	0.00035	2.586	343.5	2.982	1.376	309.9
40.00	1.50	439	4058.9	4.416	1.3824	1.6268	133	0.00029	3.031	356.4	4.620	1.467	330.4
100.00	.60	340	3899.0	4.416	1.3882	1.6093	104	0.00023	3.648	369.8	8.432	1.558	350.8
200.00	.30	280	3802.6	4.416	1.3926	1.5961	85	0.00018	4.149	377.7	13.431	1.610	362.6
400.00	.15	230	3723.2	4.416	1.4068	1.5562	70	0.00015	4.675	384.1	21.488	1.652	372.0
1000.00	.06	175	3660.1	4.416	1.4349	1.4847	55	0.00011	5.438	390.6	39.928	1.694	381.6
2000.00	.03	142	3590.9	4.416	1.4570	1.4389	45	0.00009	6.096	394.3	63.572	1.719	387.2
4000.00	.02	114	3551.2	4.416	1.4705	1.4065	36	0.00007	6.845	397.5	100.938	1.759	391.6
$R = 0.200$, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	60.00	1514	2969.7	5.216	1.3079	1.6183	402	0.00084	0.000	2.233	.209	49.3	
1.05	57.14	1497	2941.7	5.216	1.3090	1.6140	399	0.00083	.274	552.1	1.077	.539	127.4
1.20	50.00	1450	2866.8	5.216	1.3120	1.6022	389	0.00081	.533	348.6	1.289	.400	94.6
1.40	42.86	1398	2783.2	5.216	1.3155	1.5887	378	0.00078	.730	309.3	1.016	.632	149.4
1.60	37.50	1354	2713.2	5.216	1.3185	1.5772	369	0.00076	.869	299.6	1.016	.632	149.4
1.85	32.49	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	297.3	1.000	.716	169.2
2.00	30.00	1282	2601.2	5.216	1.3236	1.5584	353	0.00072	1.068	297.8	1.004	.757	179.1
4.00	15.00	1079	2290.0	5.216	1.3391	1.5045	307	0.00061	1.572	316.7	1.244	1.029	243.2
4.08	14.70	1073	2281.6	5.216	1.3395	1.5031	306	0.00061	1.585	317.4	1.256	1.035	244.7
10.00	6.00	852	1954.3	5.216	1.3559	1.4516	251	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	3.00	709	1748.8	5.216	1.3656	1.4232	213	0.00040	2.573	362.0	3.049	1.379	325.9
40.00	1.50	588	1578.0	5.216	1.3715	1.4066	179	0.00034	3.010	376.0	4.739	1.472	348.0
100.00	.60	458	1396.4	5.216	1.3771	1.3913	142	0.00026	3.619	390.5	8.679	1.565	370.0
200.00	.30	379	1286.2	5.216	1.3811	1.3807	117	0.00022	4.111	399.1	13.870	1.619	382.7
400.00	.15	312	1195.2	5.216	1.3861	1.3677	96	0.00018	4.638	406.1	22.295	1.662	392.9
1000.00	.06	242	1099.7	5.216	1.3973	1.3400	74	0.00013	5.394	413.4	41.978	1.706	403.5
2000.00	.03	198	1041.2	5.216	1.4156	1.2977	61	0.00011	6.014	417.6	67.687	1.733	409.6
4000.00	.02	161	994.0	5.216	1.4350	1.2568	50	0.00009	6.704	421.1	108.753	1.754	414.6
$R = 0.250$, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	60.00	1816	1249.3	6.015	1.2835	1.4954	481	0.00092	0.000	2.219	.207	50.3	
1.05	57.14	1797	1220.2	6.015	1.2845	1.4916	477	0.00091	.276	563.4	1.283	.398	96.6
1.20	50.00	1744	1142.1	6.015	1.2887	1.4642	467	0.00088	.538	356.1	1.073	.536	130.1
1.40	42.86	1685	1054.8	6.015	1.2901	1.4692	456	0.00086	.736	316.2	1.073	.629	154.6
1.60	37.50	1635	981.6	6.015	1.2927	1.4580	446	0.00083	.876	306.6	1.015	.629	154.6
1.85	32.49	1586	910.0	6.015	1.2955	1.4484	436	0.00081	1.000	304.5	1.000	.708	171.8
2.00	30.00	1554	864.1	6.015	1.2973	1.4414	429	0.00080	1.078	302.1	1.005	.754	183.1
4.00	15.00	1322	535.4	6.015	1.3126	1.3872	378	0.00068	1.578	325.4	1.256	1.027	249.2
4.08	14.70	1315	526.5	6.015	1.3130	1.3857	376	0.00068	1.592	326.1	1.267	1.033	250.0
10.00	6.00	1057	176.7	6.015	1.3330	1.3224	314	0.00054	2.147	355.2	2.048	1.258	305.5
20.00	3.00	866	9954.7	6.015	1.3461	1.2847	269	0.00046	2.563	373.6	3.127	1.382	335.6
40.00	1.50	740	7689.8	6.015	1.3569	1.2558	228	0.00038	2.987	388.5	4.883	1.478	358.5
100.00	.60	580	9570.0	6.015	1.3664	1.2320	181	0.00030	3.581	404.1	8.984	1.575	382.3
200.00	.30	481	9448.9	6.015	1.3717	1.2191	151	0.00025	4.064	413.3	14.394	1.630	395.8
400.00	.15	399	9348.4	6.015	1.3755	1.2100	124	0.00020	4.582	420.8	23.205	1.675	406.7
1000.00	.06	310	9241.7	6.015	1.3821	1.1948	95	0.00015	5.328	428.6	43.886	1.722	418.0
2000.00	.03	256	9177.2	6.015	1.3886	1.1805	78	0.00012	5.945	433.3	71.266	1.749	424.6
4000.00	.02	210	9124.0	6.015	1.4039	1.1482	64	0.00010	6.607	437.0	115.624	1.771	430.0
$R = 0.300$, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	60.00	2089	9932.7	6.812	1.2649	1.3928	550	0.00097	0.000	2.219	.208	.507	
1.05	57.14	2068	9903.2	6.812	1.2657	1.3898	546	0.00096	.278	568.1	1.278	.396	97.4
1.20	50.00	2011	9823.7	6.812	1.2678	1.3811	536	0.00094	.541	359.4	1.071	.533	131.3
1.40	42.86	1946	9734.8	6.812	1.2704	1.3707	524	0.00091	.741	319.4	1.013	.626	154.0
1.60	37.50	1891	9660.0	6.812	1.2727	1.3616	514	0.00089	.881	305.9	1.013	.626	154.0
1.82	33.01	1840	9590.5	6.812	1.2750	1.3527	504	0.00087	1.000	307.9	1.000	.701	172.6
2.00	30.00	1803	9539.8	6.812	1.2767	1.3460	497	0.00085	1.082	308.6	1.000	.752	184.9
4.00	15.00	1547	9201.7	6.812	1.2901	1.2972	443	0.00074	1.585	330.1	1.265	1.027	252.2
4.08	14.70	1540	9192.5	6.812	1.2906	1.2958	442	0.00073	1.598	330.8	1.278	1.032	253.8
10.00	6.00	1252	8828.7	6.812	1.3101	1.2326	374	0.00060	2.148	361.2	2.084	1.260	310.0
20.00	3.00	1059	8595.4	6.812	1.3254	1.1882	324	0.00050	2.555	380.5	3.204	1.386	341.1
40.00	1.50	891	8398.6	6.812	1.3369	1.1525	277	0.00042	2.969	390.3	5.032	1.485	365.4
100.00	.60	704	8186.3	6.812	1.3555	1.1170	224	0.00033	3.545	412.7	9.315	1.584	389.8
200.00	.30	587	8056.1	6.812	1.3607	1.1005	186	0.00027	4.015	422.5	14.975	1.642	404.1
400.00	.15	487	7947.8	6.812	1.3669	1.0868	155	0.00023	4.519	430.5	24.203	1.689	415

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P_s , lb/sq in abs	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/(lb·°K)	Viscosity, μ , poise	Thermal conductivity, k , cal/(sec·°K)	Mach number, M	Specific impulse in vacuum, I_{vac} , sec	Area ratio, E	Thrust coefficient, C_F	Specific impulse, I , lb/sec/lb
$R = 0.350$, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	60.00	2329	8892.8	7.597	1.2510	1.3038	.508	0.0099	0.000	568.1	2.199	0.000	0.0
1.05	57.14	2307	8863.2	7.597	1.2516	1.3011	.604	0.0098	.280	539.7	1.274	.205	50.7
1.20	50.00	2245	8783.7	7.597	1.2534	1.2936	.594	0.0096	.544	359.7	1.274	.394	97.4
1.40	42.86	2176	8694.6	7.597	1.2556	1.2849	.582	0.0094	.745	319.9	1.069	.532	131.3
1.60	37.50	2118	8619.6	7.597	1.2575	1.2774	.572	0.0092	.886	310.5	1.012	.624	154.2
1.81	33.18	2065	8552.7	7.597	1.2593	1.2705	.563	0.0090	1.000	308.6	1.000	.696	172.0
2.00	30.00	2023	8498.8	7.597	1.2608	1.2646	.555	0.0088	1.087	309.5	1.006	.750	185.2
4.00	15.00	1748	8157.4	7.597	1.2726	1.2211	.501	0.0078	1.590	331.6	1.273	1.024	253.0
4.08	14.70	1741	8148.1	7.597	1.2730	1.2198	.499	0.0077	1.603	332.4	1.286	1.030	254.6
10.00	6.00	1430	7777.6	7.597	1.4006	1.1616	.429	0.0064	2.150	363.7	2.114	1.261	311.5
20.00	3.00	1219	7537.8	7.597	1.3037	1.1171	.376	0.0054	2.551	383.8	3.272	1.390	343.4
40.00	1.50	1033	7334.0	7.597	1.3269	1.0765	.325	0.0046	2.955	400.2	5.170	1.491	368.3
100.00	*60	823	7112.3	7.597	1.3383	1.0347	.263	0.0036	3.515	417.4	9.636	1.593	393.6
200.00	*30	689	6975.5	7.597	1.3490	1.0110	.221	0.0030	3.970	427.7	15.552	1.653	408.4
400.00	*15	575	6861.1	7.597	1.3588	.9946	.185	0.0024	4.461	436.0	25.218	1.702	420.5
1000.00	*06	451	6738.6	7.597	1.3645	.9790	.145	0.0019	5.172	444.8	48.013	1.753	432.9
2000.00	*03	375	6664.0	7.597	1.3696	.9692	.118	0.0015	5.763	450.1	78.373	1.783	440.4
4000.00	*02	310	6602.0	7.597	1.3746	.9598	.096	0.0012	6.407	454.4	128.116	1.807	446.5
$R = 0.400$, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	60.00	2531	8050.5	8.363	1.2404	1.2259	.656	0.0040	0.000	564.6	2.193	0.000	0.0
1.05	57.14	2508	8021.3	8.363	1.2410	1.2237	.653	0.0039	.281	537.7	1.271	.205	50.4
1.20	50.00	2463	7942.8	8.363	1.2425	1.2176	.642	0.0037	.547	357.7	1.271	.393	96.8
1.40	42.86	2371	7854.5	8.363	1.2444	1.2098	.621	0.0035	.748	318.3	1.067	.530	130.6
1.60	37.50	2309	7780.4	8.363	1.2461	1.2033	.620	0.0033	.889	309.0	1.012	.623	153.3
1.80	33.18	2256	7716.2	8.363	1.2476	1.1972	.611	0.0031	1.000	307.3	1.000	.693	170.6
2.00	30.00	2209	7660.6	8.363	1.2490	1.1919	.603	0.0029	1.091	308.2	1.007	.748	184.2
4.00	15.00	1920	7321.0	8.363	1.2591	1.1547	.549	0.0020	1.594	330.7	1.280	1.023	251.9
4.08	14.70	1912	7311.7	8.363	1.2594	1.1536	.548	0.0019	1.607	331.5	1.292	1.030	253.5
10.00	6.00	1583	6940.6	8.363	1.2727	1.1009	.476	0.0007	2.151	363.4	2.138	1.262	310.8
20.00	3.00	1359	6698.7	8.363	1.2894	1.0585	.421	0.0007	2.548	383.9	3.327	1.393	343.0
40.00	1.50	1159	6491.7	8.363	1.3046	1.0178	.368	0.0004	2.945	400.8	5.287	1.496	368.3
100.00	*60	931	6264.8	8.363	1.3239	.9712	.301	0.0038	3.492	418.6	9.918	1.601	394.2
200.00	*30	784	6123.9	8.363	1.3366	.9436	.255	0.0032	3.934	429.2	16.077	1.663	409.4
400.00	*15	657	6005.5	8.363	1.3467	.9230	.214	0.0026	4.411	437.9	26.157	1.713	421.8
1000.00	*06	518	5878.1	8.363	1.3573	.9026	.168	0.0020	5.102	447.1	49.977	1.766	434.8
2000.00	*03	431	5800.3	8.363	1.3627	.8928	.139	0.0016	5.680	452.6	81.743	1.797	442.5
4000.00	*02	358	5735.5	8.363	1.3680	.8833	.113	0.0013	6.309	457.1	133.896	1.823	448.8
$R = 0.450$, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	60.00	2696	7354.5	9.102	1.2326	1.1570	.696	0.0099	0.000	568.6	2.188	0.000	0.0
1.05	57.14	2671	7325.9	9.102	1.2331	1.1550	.692	0.0099	.282	558.6	2.188	.204	49.9
1.20	50.00	2604	7249.0	9.102	1.2344	1.1496	.682	0.0097	.548	354.0	1.269	.392	95.8
1.40	42.86	2529	7162.6	9.102	1.2360	1.1434	.670	0.0095	.750	315.1	1.066	.529	129.2
1.60	37.50	2465	7089.8	9.102	1.2375	1.1377	.660	0.0093	.891	306.1	1.011	.622	151.8
1.80	33.18	2411	7028.4	9.102	1.2388	1.1326	.651	0.0092	1.000	304.4	1.000	.690	166.4
2.00	30.00	2362	6972.2	9.102	1.2401	1.1278	.643	0.0090	1.093	305.4	1.008	.747	182.4
4.00	15.00	2061	6638.0	9.102	1.2490	1.0950	.589	0.0081	1.597	328.1	1.284	1.023	249.7
4.08	14.70	2053	6628.9	9.102	1.2493	1.0940	.587	0.0080	1.610	328.9	1.297	1.029	251.3
10.00	6.00	1710	6261.7	9.102	1.2637	1.0464	.516	0.0068	2.153	361.0	2.157	1.263	308.4
20.00	3.00	1476	6021.0	9.102	1.2766	1.0076	.460	0.0059	2.547	381.8	3.370	1.395	340.6
40.00	1.50	1266	5813.8	9.102	1.2911	.9682	.405	0.0050	2.938	399.0	5.380	1.500	366.1
100.00	*60	1024	5585.4	9.102	1.3112	.9199	.334	0.0040	3.474	417.1	10.154	1.607	392.3
200.00	*30	866	5442.7	9.102	1.3250	.8901	.285	0.0033	3.906	428.0	16.525	1.670	407.9
400.00	*15	729	5322.2	9.102	1.3373	.8657	.241	0.0027	4.370	437.0	26.977	1.722	420.5
1000.00	*06	577	5192.1	9.102	1.3495	.8430	.180	0.0021	5.045	466.4	51.722	1.777	433.8
2000.00	*03	481	5112.3	9.102	1.3569	.8300	.158	0.0017	5.609	452.0	84.764	1.809	441.7
4000.00	*02	401	5045.7	9.102	1.3625	.8207	.129	0.0014	6.225	456.7	139.079	1.836	446.2
$R = 0.500$, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	60.00	2828	6769.6	9.811	1.2265	1.0967	.728	0.0098	0.000	568.6	2.184	0.000	0.0
1.05	57.14	2802	6741.8	9.811	1.2270	1.0949	.724	0.0098	.283	551.1	2.184	.204	49.9
1.20	50.00	2734	6666.9	9.811	1.2283	1.0899	.714	0.0096	.550	349.4	1.268	.392	94.5
1.40	42.86	2657	6558.8	9.811	1.2298	1.0841	.702	0.0094	.751	311.1	1.065	.528	127.5
1.60	37.50	2591	6511.8	9.811	1.2311	1.0791	.692	0.0092	.893	302.2	1.011	.621	149.8
1.79	33.44	2486	6453.1	9.811	1.2322	1.0749	.684	0.0091	1.000	300.6	1.000	.688	166.0
2.00	30.00	2486	6397.2	9.811	1.2333	1.0706	.675	0.0089	1.096	301.6	1.008	.746	180.0
4.00	15.00	2175	6070.5	9.811	1.2415	1.0511	.622	0.0080	1.599	324.4	1.288	1.022	246.6
4.08	14.70	2168	6061.5	9.811	1.2418	1.0402	.620	0.0080	1.612	325.1	1.301	1.029	248.2
10.00	6.00	1813	5701.2	9.811	1.2548	.9976	.549	0.0065	2.153	357.3	2.172	1.264	304.9
20.00	3.00	1571	5463.9	9.811	1.2667	.9619	.494	0.0060	2.545	378.1	3.304	1.397	337.1
40.00	1.50	1354	5258.9	9.811	1.2806	.9245	.436	0.0051	2.933	395.5	5.454	1.503	362.6
1000.00	*60	1102	5031.6	9.811	1.3003	.8769	.363	0.0041	3.461	413.8	10.345	1.612	388.9
2000.00	*30	936	4888.8	9.811	1.3150	.8455	.312	0.0034	3.885	424.9	16.895	1.677	404.5
4000.00	*15	790	4767.9	9.811	1.3283	.8194	.264	0.0028	4.339	434.0	27.668	1.730	417.3
1000.00	*0												

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN
[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P, lb/in ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(deg·°K·g)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec·°K·cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , lb/(sec·lb)	Area ratio, ε	Thrust coefficient, C _F , lb/sec/lb
$R = 0.600$, PERCENT FUEL = 17.35, O/F = 4.762												
1.00	60.00	3015	5841.5	11.142	1.2182	0.956	777	0.00095	0.000	0.000	0.000	0.0
1.05	57.14	2989	5815.5	11.142	1.2186	0.9542	773	0.00094	.284	534.1	2.179	.203
1.20	50.00	2916	5745.1	11.142	1.2497	0.9901	763	0.00093	.551	538.8	1.265	.391
1.40	42.86	2838	5666.0	11.142	1.2210	0.9653	751	0.00091	.754	301.8	1.054	.527
1.60	37.45	2770	5599.2	11.142	1.2222	0.9810	741	0.00089	.896	293.2	1.010	.620
1.78	33.59	2715	5545.4	11.142	1.2232	0.9774	733	0.00088	1.000	291.8	1.000	.685
2.00	30.00	2660	5491.2	11.142	1.2242	0.9737	724	0.00087	1.099	292.8	1.008	.745
4.00	15.00	2339	5182.6	11.142	1.2312	0.998	671	0.00079	1.602	315.3	1.293	1.022
4.08	14.70	2330	5174.7	11.142	1.2314	0.9991	669	0.00078	1.615	316.0	1.307	1.028
10.00	6.00	1963	4831.8	11.142	1.2426	.9136	598	0.00068	2.155	347.8	2.192	1.265
20.00	3.00	1710	4605.0	11.142	1.2533	0.8826	541	0.00060	2.543	368.5	3.452	1.399
40.00	1.50	1483	4407.9	11.142	1.2696	0.899	484	0.00052	2.927	358.5	5.559	1.507
100.00	.60	1217	4187.7	11.142	1.2643	0.8057	409	0.00042	3.444	404.2	10.621	1.618
200.00	.30	1041	4048.4	11.142	1.2695	0.7739	354	0.00035	3.856	415.5	17.444	1.685
400.00	.15	884	3929.6	11.142	1.3139	0.7664	303	0.00029	4.295	424.7	28.712	1.740
1000.00	.06	707	3800.0	11.142	1.3311	0.7170	242	0.00023	4.931	434.5	55.548	1.798
2000.00	.03	594	3719.7	11.142	1.3414	0.7007	204	0.00019	5.465	440.4	91.527	1.833
4000.00	.02	497	3652.1	11.142	1.3504	0.6874	168	0.00015	6.048	445.3	150.804	1.862
$R = 0.700$, PERCENT FUEL = 15.25, O/F = 5.556												
1.00	60.00	3128	5138.3	12.360	1.2132	0.9147	811	0.00090	0.000	0.000	0.000	0.0
1.05	57.14	3101	5113.9	12.360	1.2136	0.9135	807	0.00090	.284	516.6	2.176	.203
1.20	50.00	3029	5088.1	12.360	1.2146	0.9101	797	0.00089	.552	327.7	1.264	.390
1.40	42.86	2947	4974.0	12.360	1.2157	0.9060	785	0.00087	.755	292.0	1.063	.527
1.60	37.45	2878	4911.5	12.360	1.2168	0.9024	775	0.00085	.898	283.8	1.010	.619
1.78	35.50	2823	4861.9	12.360	1.2177	0.8993	766	0.00084	1.000	282.4	1.000	.683
2.00	30.00	2765	4810.3	12.360	1.2187	0.8960	758	0.00083	1.100	283.4	1.009	.744
4.00	15.00	2439	4520.6	12.360	1.2249	0.8755	704	0.00076	1.604	305.4	1.296	1.021
4.08	14.70	2429	4512.6	12.360	1.2251	0.8749	702	0.00076	1.617	306.2	1.310	1.028
10.00	6.00	2055	4190.3	12.360	1.2355	0.8440	631	0.00066	2.156	337.2	2.204	1.265
20.00	3.00	1797	3975.9	12.360	1.2451	0.8168	574	0.00058	2.542	357.5	3.481	1.401
40.00	1.50	1564	3788.9	12.360	1.2564	0.7879	517	0.00051	2.923	374.6	5.624	1.509
100.00	.60	1291	3579.1	12.360	1.2741	0.7473	440	0.00042	3.434	392.8	10.796	1.623
200.00	.30	1108	3455.6	12.360	1.2890	0.7171	384	0.00035	3.839	404.0	17.797	1.691
400.00	.15	946	3351.4	12.360	1.3040	0.6897	331	0.00029	4.269	413.2	29.399	1.747
1000.00	.06	760	3206.1	12.360	1.3225	0.6595	266	0.00023	4.890	423.0	57.120	1.806
2000.00	.03	640	3128.2	12.360	1.3341	0.6402	223	0.00019	5.410	428.9	94.365	1.842
4000.00	.02	537	3062.8	12.360	1.3441	0.6290	186	0.00015	5.979	433.8	155.825	1.872
$R = 0.800$, PERCENT FUEL = 13.60, O/F = 6.349												
1.00	60.00	3188	4586.9	13.470	1.2103	0.8490	835	0.00086	0.000	0.000	0.000	0.0
1.05	57.14	3161	4564.0	13.470	1.2106	0.8480	831	0.00086	.285	499.6	2.174	.203
1.20	50.00	3088	4502.9	13.470	1.2115	0.8451	821	0.00084	.553	317.0	1.263	.390
1.40	42.86	3006	4433.2	13.470	1.2126	0.8415	809	0.00083	.756	282.5	1.063	.526
1.60	37.50	2936	4374.7	13.470	1.2136	0.8382	798	0.00082	.899	274.6	1.010	.618
1.78	35.65	2881	4326.7	13.470	1.2144	0.8356	790	0.00081	1.000	275.3	1.000	.682
2.00	30.00	2823	4279.9	13.470	1.2154	0.8326	781	0.00079	1.101	274.3	1.009	.744
4.00	15.00	2493	4000.4	13.470	1.2213	0.8143	727	0.00073	1.605	295.7	1.298	1.021
4.08	14.70	2484	4000.9	13.470	1.2219	0.8137	725	0.00072	1.616	296.4	1.312	1.028
10.00	6.00	2106	3698.1	13.470	1.2311	0.7660	654	0.00053	2.156	326.7	2.212	1.266
20.00	3.00	1845	3496.4	13.470	1.2402	0.7617	597	0.00056	2.542	346.5	3.499	1.402
40.00	1.50	1609	3319.9	13.470	1.2509	0.7255	539	0.00050	2.921	363.1	5.664	1.511
100.00	.60	1333	3121.5	13.470	1.2680	0.6980	462	0.00041	3.429	381.0	10.902	1.625
200.00	.30	1148	2994.8	13.470	1.2824	0.6694	403	0.00035	3.829	392.0	18.014	1.694
400.00	.15	982	2885.1	13.470	1.2975	0.6454	350	0.00029	4.254	401.1	29.828	1.751
1000.00	.06	742	2766.6	13.470	1.3104	0.6138	284	0.00023	4.865	410.8	58.120	1.811
2000.00	.03	669	2692.0	13.470	1.3290	0.5960	239	0.00019	5.377	416.6	96.197	1.848
4000.00	.02	562	2629.2	13.470	1.3397	0.5819	200	0.00015	5.937	421.5	159.100	1.878
$R = 0.900$, PERCENT FUEL = 12.28, O/F = 7.143												
1.00	60.00	3213	4142.9	14.479	1.2086	0.7951	552	0.00082	0.000	0.000	0.000	0.0
1.05	57.14	3166	4121.5	14.479	1.2089	0.7942	548	0.00082	.285	483.8	2.173	.203
1.20	50.00	3112	4053.0	14.479	1.2094	0.7915	537	0.00081	.553	307.0	1.263	.390
1.40	42.86	3031	3998.5	14.479	1.2106	0.7883	525	0.00079	.757	273.6	1.063	.526
1.60	37.50	2961	3945.9	14.479	1.2116	0.7853	513	0.00078	.899	266.0	1.010	.618
1.78	35.72	2907	3901.7	14.479	1.2125	0.7829	506	0.00077	1.000	264.7	1.000	.681
2.00	30.00	2848	3854.9	14.479	1.2135	0.7802	497	0.00076	1.102	265.7	1.009	.744
4.00	15.00	2518	3600.9	14.479	1.2192	0.7534	742	0.00069	1.606	286.5	1.299	1.021
4.08	14.70	2508	3592.9	14.479	1.2199	0.7529	741	0.00069	1.619	287.2	1.313	1.028
10.00	6.00	2129	3308.4	14.479	1.2287	0.7374	669	0.00061	2.156	316.7	2.216	1.266
20.00	3.00	1866	3118.4	14.479	1.2374	0.7223	611	0.00056	2.541	335.9	3.209	1.402
40.00	1.50	1632	2952.2	14.479	1.2470	0.7010	553	0.00048	2.919	354.2	5.098	1.512
100.00	.60	1324	2764.7	14.479	1.2644	0.6762	476	0.00039	3.425	369.6	10.964	1.626
200.00	.30	1166	2650.1	14.479	1.2710	0.6594	418	0.00034	3.824	380.3	18.140	1.696
400.00	.15	1001	2592.1	14.479	1.2746	0.6406	363	0.00028	4.245	389.2	20.080	1.753
1000.00	.06	809	2426.7	14.479	1.2910	0.5762	285	0.00022	4.851	398.7	58.719	1.814
2000.00	.03	654	2357.0	14.479	1.2920	0.5590	250	0.00018	5.357	404.5	97.311	1.851
4000.00	.02	573	2295.1	14.479	1.2930	0.5446	210	0.00015	5.912	409.2	161.114	1.882

TABLE III. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN
[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s , lb/inch ²	Temperature, T_s , °K	Enthalpy, h_s , cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/(lb)(°K)	Thermal conductivity, k , cal/(inch)(°K)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb/second)/lb	Area ratio, ϵ	Thrust coefficient, C_f	Specific impulse, I , (lb/second)/lb
$R = 1.000$, PERCENT FUEL = 11.19, O/F = 7.937												
1.00	60.00	3217	3777.9	15.399	1.2077	0.7503	864	0.000 9	0.000	0.173	0.000	0.0 0
1.05	57.14	3190	3757.7	15.399	1.2080	0.7494	860	0.000 8	0.285	469.4	2.173	2.203 41.9
1.20	50.00	3118	3703.4	15.399	1.2088	0.7470	849	0.000 7	0.554	297.9	1.262	3.390 60.5
1.40	42.86	3036	3642.1	15.399	1.2099	0.7459	837	0.000 6	0.757	265.5	1.063	5.26 108.7
1.60	37.50	2966	3590.4	15.399	1.2108	0.7412	826	0.000 5	0.899	258.1	1.010	6.16 127.7
1.78	33.73	2912	3550.2	15.399	1.2118	0.7389	810	0.000 4	1.000	256.9	1.000	6.81 140.7
2.00	30.00	2853	3506.7	15.399	1.2125	0.7364	808	0.000 3	1.102	257.9	1.009	7.43 153.6
4.00	15.00	2523	3266.5	15.399	1.2181	0.7207	753	0.000 6	1.606	278.1	1.300	1.021 210.9
4.08	14.70	2514	3259.8	15.399	1.2183	0.7202	751	0.000 6	1.619	278.8	1.313	1.027 212.3
10.00	6.00	2135	2991.6	15.399	1.2274	0.6965	678	0.000 8	2.156	307.4	2.218	1.266 261.6
20.00	3.00	1875	2812.4	15.399	1.2360	0.6759	621	0.000 2	2.541	326.2	3.515	1.403 289.8
40.00	1.50	1638	2655.5	15.399	1.2462	0.6532	562	0.000 6	2.919	341.9	5.698	1.512 312.5
100.00	.60	1361	2478.5	15.399	1.2625	0.6070	485	0.000 8	3.424	359.0	10.997	1.627 336.2
200.00	.30	1175	2365.3	15.399	1.2764	0.5960	427	0.000 3	3.821	369.4	18.208	1.697 350.6
400.00	.15	1008	2267.8	15.399	1.2912	0.5722	372	0.000 7	4.241	378.1	30.218	1.754 362.5
1000.00	.06	815	2160.3	15.399	1.3103	0.5449	304	0.000 1	4.849	387.4	59.055	1.816 375.2
2000.00	.03	690	2093.1	15.399	1.3235	0.5280	258	0.000 8	5.347	393.0	97.944	1.853 382.9
4000.00	.02	581	2036.3	15.399	1.3348	0.5145	217	0.000 5	5.898	397.7	162.275	1.884 389.3
$R = 1.500$, PERCENT FUEL = 7.749, O/F = 11.905												
1.00	60.00	3116	2626.1	18.987	1.2082	0.6073	889	0.000 6	0.000	0.173	0.000	0.0 0
1.05	57.14	3090	2610.2	18.987	1.2085	0.6065	884	0.000 5	0.285	416.0	2.173	2.203 37.1
1.20	50.00	3019	2567.5	18.987	1.2094	0.6044	873	0.000 4	0.553	264.0	1.263	3.390 71.4
1.40	42.86	2939	2519.5	18.987	1.2105	0.6019	859	0.000 3	0.757	235.3	1.063	5.26 96.3
1.60	37.50	2872	2478.9	18.987	1.2115	0.5996	848	0.000 2	0.899	228.7	1.010	6.18 113.2
1.78	33.72	2819	2467.2	18.987	1.2121	0.5977	839	0.000 1	1.000	227.6	1.000	6.81 124.7
2.00	30.00	2762	2413.1	18.987	1.2134	0.5950	824	0.000 5	1.102	228.5	1.009	7.44 136.1
4.00	15.00	2442	2224.5	18.987	1.2184	0.5828	770	0.000 5	1.606	246.4	1.300	1.021 166.9
4.08	14.70	2433	2219.3	18.987	1.2191	0.5824	768	0.000 5	1.619	247.0	1.313	1.026 188.1
10.00	6.00	2066	2008.8	18.987	1.2282	0.5633	692	0.000 8	2.743	272.3	2.217	1.266 231.8
20.00	3.00	1813	1888.3	18.987	1.2388	0.5466	632	0.000 3	2.542	286.9	3.511	1.402 256.8
40.00	1.50	1584	1745.2	18.987	1.2467	0.5289	573	0.000 8	2.920	302.9	5.691	1.512 276.9
100.00	.60	1315	1606.5	18.987	1.2624	0.5035	495	0.000 1	3.425	318.0	10.982	1.627 297.9
200.00	.30	1136	1517.7	18.987	1.2771	0.4843	439	0.000 7	3.824	327.2	18.188	1.696 310.6
400.00	.15	975	1441.2	18.987	1.2898	0.4658	384	0.000 3	4.244	334.9	30.198	1.754 321.1
1000.00	.06	789	1356.9	18.987	1.3002	0.4442	317	0.000 8	4.846	343.1	59.073	1.815 332.3
2000.00	.03	669	1304.1	18.987	1.3212	0.4205	271	0.000 5	5.347	348.1	98.060	1.852 339.2
4000.00	.02	564	1259.5	18.987	1.3324	0.4190	230	0.000 3	5.896	352.3	162.595	1.883 344.8
$R = 2.000$, PERCENT FUEL = 5.927, O/F = 15.873												
1.00	60.00	2966	2016.0	21.453	1.2116	0.5304	886	0.000 7	0.000	0.173	0.000	0.0 0
1.05	57.14	2941	2002.7	21.453	1.2119	0.5297	884	0.000 7	0.285	381.8	2.175	2.203 34.1
1.20	50.00	2873	1966.7	21.453	1.2129	0.5277	870	0.000 6	0.553	242.3	1.264	3.390 65.5
1.40	42.86	2766	1926.3	21.453	1.2141	0.5253	856	0.000 5	0.756	215.9	1.063	5.26 88.4
1.60	37.50	2731	1892.1	21.453	1.2171	0.5232	844	0.000 4	0.898	209.8	1.010	6.19 103.9
1.78	33.56	2679	1865.1	21.453	1.2160	0.5215	834	0.000 3	1.000	208.8	1.000	6.83 114.6
2.00	30.00	2625	1836.7	21.453	1.2169	0.5196	824	0.000 2	1.101	209.6	1.009	7.44 124.9
4.00	15.00	2316	1678.3	21.453	1.2220	0.5079	763	0.000 8	1.604	225.9	1.297	1.021 171.4
4.08	14.70	2308	1673.9	21.453	1.2232	0.5076	761	0.000 7	1.618	226.4	1.311	1.028 172.5
10.00	6.00	1954	1497.4	21.453	1.2327	0.4906	682	0.000 1	2.156	249.5	2.208	1.265 212.4
20.00	3.00	1711	1379.8	21.453	1.2416	0.4760	622	0.000 7	2.543	264.6	3.492	1.401 235.3
40.00	1.50	1492	1277.1	21.453	1.2517	0.4607	562	0.000 2	2.923	277.3	5.650	1.510 253.6
100.00	.60	1256	1161.6	21.453	1.2671	0.4394	486	0.000 7	3.433	290.9	10.878	1.624 272.7
200.00	.30	1065	1087.9	21.453	1.2801	0.4233	421	0.000 3	3.835	299.3	17.986	1.693 284.2
400.00	.15	912	1024.5	21.453	1.2935	0.4082	378	0.000 2	4.259	306.2	29.822	1.750 293.7
1000.00	.06	737	954.7	21.453	1.3114	0.3901	313	0.000 6	4.868	313.7	58.249	1.810 303.9
2000.00	.03	624	911.1	21.453	1.3241	0.3764	269	0.000 3	5.374	318.2	96.601	1.847 310.1
4000.00	.02	525	874.3	21.453	1.3356	0.3685	229	0.000 1	5.927	321.9	160.027	1.877 315.2
$R = 3.000$, PERCENT FUEL = 4.031, O/F = 23.810												
1.00	60.00	2655	1381.4	24.532	1.2209	0.4476	851	0.000 7	0.000	0.173	0.000	0.0 0
1.05	57.14	2632	1371.0	24.532	1.2213	0.4470	847	0.000 6	0.283	337.8	2.181	2.204 30.1
1.20	50.00	2569	1342.8	24.532	1.2224	0.4452	834	0.000 6	0.551	214.2	1.266	3.391 57.9
1.40	42.86	2498	1311.2	24.532	1.2231	0.4430	820	0.000 5	0.753	190.8	1.064	5.26 78.2
1.60	37.50	2437	1294.5	24.532	1.2249	0.4411	807	0.000 4	0.895	185.4	1.010	6.20 91.8
1.78	33.56	2368	1262.4	24.532	1.2260	0.4393	797	0.000 3	1.000	186.4	1.000	6.86 101.6
2.00	30.00	2339	1241.4	24.532	1.2270	0.4370	787	0.000 2	1.098	185.1	1.000	7.45 110.4
4.00	15.00	2024	1118.2	24.532	1.2350	0.4272	723	0.000 8	1.601	199.2	1.292	1.022 191.3
4.08	14.70	2046	1114.8	24.532	1.2342	0.4269	721	0.000 8	1.615	199.7	1.305	1.028 192.3
10.00	6.00	1721	978.3	24.532	1.2448	0.4119	641	0.000 3	2.155	219.7	2.187	1.264 187.3
20.00	3.00	1499	888.0	24.532	1.2540	0.3995	581	0.000 9	2.546	232.7	3.443	1.399 207.2
40.00	1.50	1300	809.6	24.532	1.2646	0.3872	523	0.000 6	2.931	243.6	5.545	1.506 223.1
100.00	.60	1068	721.9	24.532	1.2800	0.3703	450	0.000 1	3.451	255.3	10.611	1.617 239.5
200.00	.30	916	666.3	24.532	1.2924	0.3580	398	0.000 8	3.863	262.4	17.467	1.684 249.4
400.00	.15	761	618.8	24.532	1.3026	0.3460	349	0.000 6	4.249	266.3	26.839	1.739 257.6
1000.00	.06	627	566.7	24.532	1.3230	0.3318	269	0.000 5	4.924	274.5	56.029	1.798 266.3

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR
 LIQUID HYDROGEN WITH LIQUID OXYGEN
 [Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s , lb/sq.in. abs	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	Isoentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb/sec)/lb	Area ratio, ϵ	Thrust coefficient, C_f	Specific impulse, I , (lb/sec)/lb
$R = 4.000, \text{ PERCENT FUEL} = 3.054, \text{ O/F} = 31.746$													
1.00	60.00	2347	1054.4	26.257	1.2321	0.4017	798	0.00040	0.000			0.000	0.00
1.05	57.14	2326	1045.8	26.257	1.2326	0.4010	794	0.00039	.282	306.9	2.188	.204	27.4
1.20	50.00	2268	1022.6	26.257	1.2339	0.3992	781	0.00039	.548	194.5	1.269	.392	52.6
1.40	42.86	2202	995.6	26.257	1.2355	0.3971	766	0.00038	.750	173.1	1.066	.529	71.0
1.60	37.50	2147	974.5	26.257	1.2368	0.3953	754	0.00037	.892	168.2	1.011	.621	83.4
1.80	33.42	2100	956.0	26.257	1.2380	0.3937	743	0.00036	1.000	167.3	1.000	.690	92.5
2.00	30.00	2057	939.0	26.257	1.2391	0.3922	733	0.00036	1.094	167.8	1.008	.747	100.2
4.00	15.00	1796	838.1	26.257	1.2469	0.3822	669	0.00032	1.598	180.3	1.285	1.023	137.2
4.08	14.70	1789	835.3	26.257	1.2471	0.3819	667	0.00032	1.611	180.7	1.298	1.029	138.1
10.00	6.00	1493	724.3	26.257	1.2505	0.3685	588	0.00027	2.155	198.5	2.162	1.263	169.5
20.00	3.00	1292	651.4	26.257	1.2604	0.3577	530	0.00024	2.549	210.0	3.387	1.396	187.3
40.00	1.50	1113	598.3	26.257	1.2793	0.3467	475	0.00021	2.941	219.6	5.428	1.501	201.4
100.00	.60	908	518.5	26.257	1.2990	0.3323	406	0.00017	3.471	229.8	10.316	1.610	215.9
200.00	.30	773	474.5	26.257	1.3079	0.3215	357	0.00015	3.893	236.0	16.892	1.674	224.6
400.00	.15	655	437.1	26.257	1.3212	0.3113	312	0.00013	4.342	241.1	27.741	1.728	231.8
1000.00	.06	522	396.4	26.257	1.3386	0.2992	258	0.00010	4.990	246.5	53.515	1.784	239.3
2000.00	.03	437	371.3	26.257	1.3510	0.2913	221	0.00009	5.531	249.7	87.939	1.817	243.8
4000.00	.02	364	350.4	26.257	1.3601	0.2859	187	0.00007	6.129	252.3	144.427	1.845	247.5
$R = 5.000, \text{ PERCENT FUEL} = 2.458, \text{ O/F} = 39.683$													
1.00	60.00	2062	855.0	27.299	1.2440	0.3711	740	0.00034	0.000			0.000	0.00
1.05	57.14	2042	847.4	27.299	1.2445	0.3705	735	0.00034	.281	282.0	2.195	.205	25.2
1.20	50.00	1989	828.1	27.299	1.2459	0.3668	722	0.00033	.546	178.6	1.272	.394	48.4
1.40	42.86	1929	806.1	27.299	1.2476	0.3668	708	0.00032	.747	158.9	1.068	.531	65.2
1.60	37.50	1879	787.6	27.299	1.2491	0.3650	696	0.00032	.888	154.3	1.012	.623	76.6
1.80	33.28	1835	771.5	27.299	1.2505	0.3634	684	0.00031	1.000	153.4	1.000	.694	85.2
2.00	30.00	1797	757.8	27.299	1.2517	0.3620	675	0.00031	1.050	153.8	1.007	.748	92.0
4.00	15.00	1560	673.2	27.299	1.2800	0.3528	612	0.00027	1.594	165.1	1.279	1.024	125.8
4.08	14.70	1554	670.9	27.299	1.2803	0.3525	610	0.00027	1.607	165.4	1.292	1.030	126.6
10.00	6.00	1287	578.5	27.299	1.2752	0.3399	534	0.00023	2.154	181.4	2.138	1.262	155.1
20.00	3.00	1107	518.2	27.299	1.2840	0.3300	479	0.00020	2.553	191.7	3.333	1.393	171.2
40.00	1.50	948	466.4	27.299	1.2943	0.3201	427	0.00018	2.950	200.2	5.313	1.496	183.9
100.00	.60	766	409.5	27.299	1.3111	0.3068	365	0.00014	3.491	209.2	10.027	1.602	196.9
200.00	.30	648	373.8	27.299	1.3244	0.2972	317	0.00012	3.924	214.6	16.328	1.665	204.6
400.00	.15	545	343.8	27.299	1.3380	0.2881	276	0.00010	4.387	219.1	26.662	1.716	210.9
1000.00	.06	431	311.4	27.299	1.3550	0.2779	226	0.00008	5.058	223.8	51.055	1.770	217.5
2000.00	.03	359	291.5	27.299	1.3642	0.2726	192	0.00007	5.625	226.6	83.484	1.802	221.4
4000.00	.02	298	275.0	27.299	1.3704	0.2693	162	0.00006	6.250	228.8	136.601	1.828	224.7

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_e/P	Static pressure, P_e , lb/in ² atm	Temperature, T_e , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/(g·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec·°K·cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/(lb·sec)/lb	Area ratio, ϵ	Thrust coefficient, C_F , lb/(lb·sec)/lb	Specific impulse, I , sec
$R = 0.150$, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	150.00	1183	5313.5	4.416	1.3396	1.7753	.314	0.00073	0.000	0.000	0.000	0.000	0.0
1.05	142.86	1168	5287.7	4.416	1.3406	1.7710	.311	0.00073	0.271	530.1	2.250	.210	47.4
1.20	125.00	1129	5218.6	4.416	1.3436	1.7597	.303	0.00070	0.271	534.2	1.297	.403	90.8
1.40	107.14	1052	5141.8	4.416	1.3469	1.7472	.293	0.00068	0.721	296.1	1.081	.543	122.2
1.60	93.75	1049	5077.7	4.416	1.3497	1.7369	.285	0.00066	0.860	285.6	1.018	.636	143.2
1.87	80.42	1008	5006.8	4.416	1.3526	1.7257	.276	0.00063	1.000	284.1	1.000	.725	163.4
2.00	75.00	989	4972.9	4.416	1.3550	1.7120	.274	0.00062	1.059	284.4	1.003	.761	171.5
4.00	57.50	824	4693.9	4.416	1.3651	1.6622	.234	0.00052	1.566	301.7	1.233	1.031	232.3
10.00	15.00	643	4392.5	4.416	1.3748	1.6505	.188	0.00042	2.152	327.5	1.974	1.257	483.1
10.21	14.70	639	4386.6	4.416	1.3750	1.6501	.187	0.00041	2.165	328.1	1.997	1.261	284.0
20.00	7.50	552	4209.8	4.416	1.3794	1.6394	.157	0.00035	2.586	343.5	2.982	1.376	309.9
40.00	3.75	439	4058.9	4.416	1.3824	1.6268	.133	0.00029	3.031	356.4	4.620	1.467	330.4
100.00	1.50	340	3899.0	4.416	1.3882	1.6093	.104	0.00023	3.648	369.8	8.432	1.558	350.8
200.00	.75	260	3802.6	4.416	1.3926	1.5951	.05	0.00018	4.416	377.7	13.431	1.610	362.6
400.00	.38	230	3723.4	4.416	1.4000	1.5556	.070	0.00015	4.675	384.1	21.488	1.652	372.0
1000.00	.15	175	3640.1	4.416	1.4349	1.4847	.055	0.00011	5.458	390.6	39.928	1.694	381.6
2000.00	.08	142	3570.9	4.416	1.4529	1.4389	.045	0.00009	6.096	394.3	62.572	1.719	387.2
4000.00	.04	114	3551.2	4.416	1.4405	1.4065	.036	0.00007	6.845	397.3	100.938	1.739	391.6
$R = 0.200$, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	150.00	1514	2969.7	5.216	1.3079	1.6183	.402	0.00004	0.000	0.000	0.000	0.000	0.0
1.05	142.86	1497	2941.7	5.216	1.3090	1.6140	.399	0.00003	.274	552.2	2.233	.209	49.3
1.20	125.00	1420	2800.8	5.216	1.3120	1.6022	.389	0.00001	.533	348.6	1.289	.400	94.6
1.40	107.14	1398	2783.2	5.216	1.3155	1.5887	.378	0.00078	.730	309.3	1.077	.539	127.4
1.60	93.75	1354	2715.2	5.216	1.3185	1.5772	.369	0.00076	.869	299.6	1.016	.632	149.4
1.83	81.23	1307	2640.5	5.216	1.3217	1.5651	.359	0.00073	1.000	297.3	1.000	.715	169.2
2.00	75.00	1282	2601.1	5.216	1.3236	1.5584	.353	0.00072	1.058	297.8	1.004	.757	179.1
4.00	57.50	1079	2490.0	5.216	1.3351	1.5046	.307	0.00001	1.774	316.7	1.244	1.029	243.2
10.00	15.00	824	1924.3	5.216	1.3220	1.4210	.451	0.00008	2.140	344.7	2.009	1.257	297.2
10.21	14.70	807	1947.7	5.216	1.3220	1.4206	.450	0.00008	2.161	345.3	2.033	1.261	298.2
20.00	7.50	709	1746.8	5.216	1.3050	1.4252	.415	0.00004	2.473	362.0	3.049	1.379	325.9
40.00	3.75	588	1578.0	5.216	1.3715	1.4066	.179	0.00004	3.010	376.0	4.739	1.472	348.0
100.00	1.50	458	1396.3	5.216	1.3771	1.3915	.142	0.00026	3.619	390.5	8.679	1.565	370.0
200.00	.75	379	1266.2	5.216	1.3831	1.3807	.117	0.00022	4.111	399.1	15.870	1.619	382.7
400.00	.38	312	1195.2	5.216	1.3861	1.3677	.096	0.00018	4.638	406.1	22.295	1.662	392.9
1000.00	.15	242	1099.0	5.216	1.3973	1.3400	.074	0.00013	5.393	413.4	41.979	1.706	403.5
2000.00	.08	198	1041.1	5.216	1.4156	1.2977	.061	0.00011	6.014	417.6	67.687	1.733	409.6
4000.00	.04	161	993.9	5.216	1.4330	1.2926	.050	0.00009	6.704	421.1	108.754	1.754	414.6
$R = 0.250$, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	150.00	1816	1249.5	6.016	1.2835	1.4955	.481	0.00002	0.000	0.000	0.000	0.000	0.0
1.05	142.86	1797	1220.4	6.016	1.2844	1.4917	.477	0.0001	.276	563.4	2.219	.207	50.3
1.20	125.00	1744	1142.1	6.016	1.2910	1.4914	.467	0.00049	.536	556.1	1.283	.398	96.6
1.40	107.14	1605	1054.6	6.016	1.2940	1.4893	.450	0.00006	.736	516.3	1.073	.536	130.1
1.60	93.75	1635	981.5	6.016	1.2947	1.4850	.440	0.00005	.876	506.6	1.015	.629	152.6
1.83	81.23	1566	910.0	6.016	1.2974	1.4845	.436	0.00001	1.000	504.5	1.000	.708	171.8
2.00	75.00	1554	864.0	6.016	1.2975	1.4845	.429	0.00000	1.076	505.1	1.005	.754	185.1
4.00	57.50	1322	555.3	6.016	1.3125	1.3937	.378	0.00008	1.578	325.5	1.256	1.027	249.3
10.00	15.00	1057	176.5	6.016	1.3530	1.3227	.314	0.00005	2.147	355.3	2.048	1.256	303.5
10.21	14.70	1052	1493.3	6.016	1.3530	1.3212	.312	0.00004	2.159	355.8	2.072	1.265	308.5
20.00	7.50	807	954.6	6.016	1.3581	1.2648	.269	0.00006	2.453	373.6	3.127	1.382	332.7
40.00	3.75	740	7686.0	6.016	1.3570	1.2579	.220	0.00003	2.907	388.6	4.883	1.478	356.9
100.00	1.50	580	958.7	6.016	1.3663	1.2520	.181	0.00000	3.281	404.1	8.985	1.573	382.3
200.00	.75	481	944.6	6.016	1.3717	1.2519	.151	0.00002	4.064	413.3	14.392	1.630	395.9
400.00	.38	399	934.8	6.016	1.3720	1.2410	.124	0.00000	4.382	420.8	23.206	1.675	400.7
1000.00	.15	310	9241.3	6.016	1.3821	1.1940	.095	0.00015	5.327	428.7	43.889	1.722	418.0
2000.00	.08	256	9176.7	6.016	1.3855	1.1805	.078	0.00012	5.945	433.3	71.271	1.749	424.7
4000.00	.04	210	9123.6	6.016	1.4039	1.1482	.064	0.00010	6.606	437.1	115.634	1.771	430.1
$R = 0.300$, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	150.00	2092	9932.7	6.813	1.2648	1.3932	.550	0.00007	0.000	0.000	0.000	0.000	0.0
1.05	142.86	2071	9903.1	6.813	1.2655	1.3930	.546	0.00006	.278	568.3	2.408	.206	50.8
1.20	125.00	2013	9823.6	6.813	1.2670	1.3814	.536	0.00004	.542	359.6	1.278	.396	97.5
1.40	107.14	1949	9749.5	6.813	1.2703	1.3731	.524	0.00001	.741	314.6	1.071	.533	131.3
1.60	93.75	1874	9659.7	6.813	1.2742	1.3619	.514	0.00005	.881	310.0	1.013	.626	154.1
1.83	81.23	1843	9570.4	6.813	1.2744	1.3520	.504	0.00007	1.000	306.1	1.000	.701	174.6
2.00	75.00	1602	9239.4	6.813	1.2765	1.3463	.497	0.00002	1.686	308.8	1.006	.752	185.0
4.00	57.50	1549	9200.4	6.813	1.2893	1.2976	.444	0.00004	1.559	330.4	1.266	1.025	256.4
10.00	15.00	1224	8827.4	6.813	1.3094	1.2329	.374	0.00000	2.140	361.4	4.084	1.260	310.1
10.21	14.70	1240	8819.7	6.813	1.3103	1.2315	.373	0.00000	2.160	362.1	4.110	1.264	311.2
20.00	7.50	1061	8574.8	6.813	1.3222	1.1885	.324	0.00000	2.455	380.8	3.204	1.388	341.3
40.00	3.75	893	8396.8	6.813	1.3307	1.1527	.278	0.00002	2.969	395.6	5.034	1.485	365.6
100.00	1.50	703	8184.1	6.813	1.3533	1.1172	.223	0.00003	3.245	413.0	4.318	1.284	390.1
200.00	.75	586	8035.6	6.813	1.3600	1.1005	.186	0.00007	4.014	422.0	4.981	1.644	404.3

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN
[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/in ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, Y	Specific heat, c _p , cal/g·°K	Viscosity, μ, micro poises	Thermal conductivity, k, cal/sec/in ² °K/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , sec	Area ratio, ε	Thrust coefficient, C _F , lb/sec/lb	Specific impulse, I, lb/sec/lb
R = 0.350, PERCENT FUEL = 26447, O/F = 2.778													
1.00	150.00	2337	8892.8	7.604	1.2505	1.3047	610	0.00099	0.000	2.199	0.000	0.00	0.00
1.05	142.86	2310	8893.8	7.604	1.2511	1.3020	609	0.00099	2.280	569.0	2.199	.205	50.8
1.20	125.00	2259	8763.4	7.604	1.2529	1.2949	599	0.00097	.544	360.3	1.274	.394	97.6
1.40	107.14	2182	8693.9	7.604	1.2551	1.2892	588	0.00094	.745	320.4	1.069	.532	131.5
1.60	95.75	2126	8618.7	7.604	1.2570	1.2784	574	0.00092	.886	311.0	1.012	.624	154.4
1.81	82.47	2074	8551.7	7.604	1.2587	1.2713	566	0.00090	1.000	309.2	1.000	.696	172.3
2.00	75.00	2031	8497.5	7.604	1.2602	1.2656	556	0.00089	1.087	310.0	1.007	.749	185.5
4.00	37.50	1756	8154.9	7.604	1.2740	1.2223	504	0.00078	1.390	332.2	1.274	1.024	253.4
10.00	15.00	1436	7773.7	7.604	1.2899	1.1627	431	0.00064	4.150	364.4	2.115	1.261	312.1
10.21	14.70	1430	7766.0	7.604	1.2904	1.1614	429	0.00064	4.162	365.0	2.142	1.265	313.1
20.00	7.50	1223	7532.9	7.604	1.3020	1.1182	377	0.00055	2.551	384.5	3.274	1.390	344.0
40.00	3.75	1039	7328.2	7.604	1.3202	1.0774	326	0.00046	2.955	401.0	5.175	1.491	369.0
100.00	1.50	828	7105.5	7.604	1.3377	1.0353	264	0.00036	3.514	418.2	9.648	1.594	394.4
200.00	.75	634	6968.0	7.604	1.3485	1.0112	223	0.00030	3.369	428.5	15.575	1.654	409.2
400.00	.38	579	6833.0	7.604	1.3563	.9948	166	0.00025	4.459	436.9	25.259	1.703	421.3
1000.00	.15	424	6729.5	7.604	1.3642	.9790	146	0.00019	5.169	445.7	48.98	1.753	433.8
2000.00	.08	371	6524.9	7.604	1.3692	.9693	119	0.00015	5.760	451.0	78.522	1.783	441.3
4000.00	.04	312	6592.2	7.604	1.3742	.9596	97	0.00012	6.403	455.3	128.377	1.808	447.4
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	150.00	2553	8050.9	8.379	1.2395	1.2276	660	0.00101	0.000	2.192	0.000	0.00	0.00
1.05	142.86	2529	8024.1	8.379	1.2400	1.2224	656	0.00100	4.81	266.4	2.192	.205	50.6
1.20	125.00	2464	7942.1	8.379	1.2415	1.2192	646	0.00098	5.47	258.9	1.271	.393	97.1
1.40	107.14	2391	7695.3	8.379	1.2493	1.2116	634	0.00096	.748	319.3	1.067	.530	131.0
1.60	93.75	2369	7710.0	8.379	1.2470	1.2052	624	0.00094	.889	310.1	1.012	.623	153.8
1.80	83.31	2276	7714.2	8.379	1.2465	1.1992	615	0.00092	1.000	308.3	1.000	.692	171.1
2.00	75.00	2229	7658.0	8.379	1.2479	1.1938	607	0.00090	1.091	309.2	1.007	.748	184.8
4.00	37.50	1930	7316.0	8.379	1.2578	1.1970	553	0.00080	1.599	331.9	1.280	1.023	252.8
10.00	15.00	1599	6932.6	8.379	1.2738	1.1033	480	0.00067	2.152	364.8	2.141	1.262	311.9
10.21	14.70	1592	6924.9	8.379	1.2742	1.1021	479	0.00067	2.163	365.4	2.168	1.267	313.0
20.00	7.50	1373	6688.4	8.379	1.2879	1.0609	425	0.00058	2.548	385.4	3.332	1.393	344.2
40.00	3.75	1173	6479.7	8.379	1.3030	1.0400	371	0.00049	2.944	402.4	5.298	1.496	369.7
100.00	1.50	943	6250.6	8.379	1.3244	.9720	304	0.00039	3.490	420.3	9.946	1.602	395.7
200.00	.75	794	6108.4	8.379	1.3321	.9494	228	0.00032	3.931	431.0	16.131	1.664	411.1
400.00	.38	660	5988.4	8.379	1.3459	.9260	217	0.00026	4.406	394.8	26.255	1.714	423.6
1000.00	.15	525	5855.6	8.379	1.3502	.9029	170	0.00020	5.095	449.0	50.189	1.757	436.6
2000.00	.08	437	5780.8	8.379	1.3517	.8948	141	0.00017	5.672	454.5	82.113	1.799	444.4
4000.00	.04	365	5715.2	8.379	1.3670	.8833	115	0.00014	6.299	459.1	134.543	1.824	450.8
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	150.00	2733	7354.5	9.133	1.2310	1.1595	701	0.00100	0.000	2.187	0.000	0.00	0.00
1.05	142.86	2708	7325.6	9.133	1.2315	1.1576	696	0.00100	2.282	261.5	2.187	.204	50.1
1.20	125.00	2640	7247.9	9.133	1.2326	1.1521	688	0.00098	.549	355.9	1.269	.392	96.3
1.40	107.14	2564	7180.0	9.133	1.2346	1.1459	676	0.00096	.750	316.8	1.066	.529	129.9
1.60	93.75	2500	7087.1	9.133	1.2359	1.1404	666	0.00094	.892	307.7	1.011	.621	152.5
1.79	83.55	2446	7025.3	9.133	1.2371	1.1355	657	0.00092	1.000	306.0	1.000	.669	169.2
2.00	75.00	2395	6968.2	9.133	1.2383	1.1307	649	0.00091	1.090	307.0	1.008	.747	183.3
4.00	37.50	2072	6630.4	9.133	1.2471	1.0982	595	0.00082	1.597	329.9	1.285	1.023	251.0
10.00	15.00	1738	6249.2	9.133	1.2614	1.0500	522	0.00069	2.153	363.2	2.161	1.263	310.1
10.21	14.70	1730	6241.5	9.133	1.2617	1.0489	521	0.00069	2.165	363.8	2.189	1.268	311.2
20.00	7.50	1501	6005.3	9.133	1.2741	1.0114	467	0.00060	2.546	384.1	3.379	1.396	342.6
40.00	3.75	1289	5797.1	9.133	1.2884	.9720	411	0.00051	2.937	401.5	5.399	1.500	368.4
100.00	1.50	1042	5503.1	9.133	1.3084	.9231	341	0.00041	3.471	419.9	10.202	1.608	394.8
200.00	.75	885	5417.9	9.133	1.3124	.8924	291	0.00034	3.901	430.9	16.518	1.676	410.5
400.00	.38	745	5295.2	9.133	1.3349	.8673	240	0.00028	4.362	440.0	27.151	1.724	423.3
1000.00	.15	590	5162.6	9.133	1.3470	.8438	194	0.00022	5.033	449.5	52.106	1.777	436.7
2000.00	.08	493	5084.2	9.133	1.3523	.8300	162	0.00018	5.593	452.2	55.445	1.814	444.8
4000.00	.04	410	5013.2	9.133	1.3600	.8207	132	0.00014	6.207	460.0	140.269	1.838	451.4
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	150.00	2881	6769.6	9.859	1.2244	1.0999	736	0.00099	0.000	2.183	0.000	0.00	0.00
1.05	142.86	2852	6741.8	9.859	1.2244	1.0981	732	0.00099	4.283	554.9	2.183	.204	49.5
1.20	125.00	2788	6665.5	9.859	1.2260	1.0932	722	0.00097	.550	351.8	1.267	.392	95.2
1.40	107.14	2707	6590.2	9.859	1.2273	1.0975	710	0.00095	.752	313.3	1.055	.528	128.4
1.60	93.75	2641	6508.0	9.859	1.2289	1.0924	700	0.00093	.894	304.4	1.011	.620	150.8
1.79	83.55	2580	6447.1	9.859	1.2299	1.0793	694	0.00092	1.000	304.8	1.000	.687	167.0
2.00	75.00	2353	6371.7	9.859	1.2310	1.0491	682	0.00091	1.096	303.8	1.008	.748	181.3
4.00	37.50	2240	6000.4	9.859	1.2309	1.0392	630	0.00082	1.560	326.8	1.289	1.022	246.5
10.00	15.00	1854	5684.8	9.859	1.2421	1.0024	558	0.00070	2.154	360.2	2.177	1.264	307.2
10.21	14.70	1840	5677.1	9.859	1.2424	1.0014	556	0.00070	2.166	360.4	2.205	1.268	308.3
20.00	7.50	1609	5443.4	9.859	1.2503	.9670	504	0.00061	2.545	381.3	3.416	1.398	339.7
40.00	3.75	1388	5234.1	9.859	1.2578	.9297	445	0.00053	2.932	398.8	5.481	1.504	365.5
1000.00	1.50	1152	5001.9	9.859	1.2694	.8817	372	0.00042	3.457	417.5	10.413	1.613	392.2
2000.00	.75	963	4855.6	9.859	1.2712	.8693	320	0.00035	3.678	428.8	17.030	1.679	408.1
4000.00	.38	812	4731.6	9.859	1.2847	.8623	272	0.00029	4.328	438.1	27.924	1.732	421.1
1000.00													

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OX GEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, p , lb/in. ²	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/(kg·°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec·°K)cm	Mach number, M	Specific impulse in vacuum, I_{vac} , lb(lb/sec)/lb	Area ratio, ϵ	Thrust coefficient, C_f	Specific impulse, I , lb(sec)/lb
$R = 0.600$; PERCENT FUEL = 17.35; O/F = 4.762													
1.00	150.00	3097	5841.6	11.228	1.2152	0.9995	768	0.00096	0.284	539.3	2.177	0.000	0.0
1.05	142.86	3070	5615.0	11.228	1.2155	0.9981	765	0.00096	0.284	539.3	2.177	0.03	45.1
1.20	125.00	2998	5743.3	11.228	1.2160	0.9942	774	0.00094	0.552	342.1	1.264	0.391	94.5
1.40	107.14	2917	5662.5	11.228	1.2174	0.9895	763	0.00092	0.759	304.8	1.064	0.527	129.8
1.60	93.75	2848	5594.5	11.228	1.2189	0.9853	753	0.00091	0.897	296.2	1.010	0.619	146.6
1.78	84.08	2793	5540.1	11.228	1.2199	0.9819	745	0.0009	1.000	294.7	1.000	0.684	164.0
2.00	75.00	2736	5484.2	11.228	1.2209	0.9782	736	0.00088	1.100	295.8	1.009	0.744	176.3
4.00	37.50	2410	5169.0	11.228	1.2215	0.9550	683	0.00085	1.603	318.6	1.295	1.021	241.9
10.00	15.00	2027	4802.6	11.228	1.2303	0.9191	611	0.00070	4.152	351.7	4.199	1.262	299.6
10.21	14.70	2019	4802.6	11.228	1.2306	0.9189	610	0.00070	4.167	354.4	4.228	1.269	300.7
20.00	7.50	1770	4575.3	11.228	1.2405	0.8893	529	0.00062	2.343	372.8	3.469	1.400	331.7
40.00	3.75	1538	4374.7	11.228	1.2604	0.8772	498	0.00054	2.925	390.4	5.598	1.508	357.3
100.00	1.50	1266	4147.8	11.228	1.2785	0.8168	423	0.00044	3.439	409.5	10.724	1.621	363.9
200.00	.75	1086	4003.7	11.228	1.2933	0.7804	368	0.00037	3.846	420.8	17.650	1.688	359.9
400.00	.38	925	3880.6	11.228	1.3080	0.7516	316	0.00031	4.280	430.3	29.113	1.744	413.1
1000.00	.15	742	3745.9	11.228	1.3257	0.7204	253	0.00024	4.907	440.4	56.470	1.803	427.0
2000.00	.08	624	3662.3	11.228	1.3366	0.7028	212	0.00020	5.433	446.5	93.204	1.838	435.5
4000.00	.04	523	3592.1	11.228	1.3459	0.6886	176	0.00016	6.008	451.5	153.804	1.868	442.4
$R = 0.700$; PERCENT FUEL = 15.25; O/F = 5.556													
1.00	150.00	3231	5138.3	12.482	1.2076	0.9187	825	0.00092	0.000	0.000	0.000	0.000	0.0
1.05	142.86	3203	5113.3	12.482	1.2099	0.9175	822	0.00092	0.285	522.5	2.174	0.03	46.6
1.20	125.00	3130	5040.0	12.482	1.2108	0.9143	811	0.00090	0.553	531.0	1.263	0.390	89.6
1.40	107.14	3047	4970.2	12.482	1.2119	0.9105	800	0.00089	0.756	495.4	1.063	0.526	120.9
1.60	93.75	2770	4908.4	12.482	1.2129	0.9070	789	0.00087	0.899	487.2	1.010	0.618	142.1
1.78	84.26	2791	4902.1	12.482	1.2137	0.9041	781	0.00086	1.000	485.0	1.000	0.684	156.7
2.00	75.00	2862	4802.5	12.482	1.2146	0.9009	773	0.00085	1.102	486.9	1.009	0.744	170.9
4.00	37.50	2528	4502.4	12.482	1.2206	0.8810	720	0.00078	1.605	309.3	1.299	1.021	234.7
10.00	15.00	2136	4169.8	12.482	1.2303	0.8504	648	0.00068	2.156	341.8	2.213	1.266	290.9
10.21	14.70	2128	4150.8	12.482	1.2306	0.8497	647	0.00068	2.168	342.4	2.242	1.270	291.9
20.00	7.50	1873	3944.8	12.482	1.2393	0.8244	592	0.00061	2.542	362.5	3.502	1.402	322.3
40.00	3.75	1634	3751.6	12.482	1.2500	0.7960	535	0.00053	2.920	380.0	5.671	1.511	347.4
100.00	1.50	1354	3534.1	12.482	1.2670	0.7556	459	0.00044	3.427	398.7	10.922	1.622	372.6
200.00	.75	1167	3559.2	12.482	1.2813	0.7241	402	0.00037	3.862	410.4	18.023	1.694	389.5
400.00	.38	999	3272.9	12.482	1.2905	0.6964	348	0.00031	4.251	419.7	29.905	1.751	402.6
1000.00	.15	806	3144.6	12.482	1.3121	0.6644	282	0.00024	4.881	429.9	58.305	1.814	416.5
2000.00	.08	681	3062.0	12.482	1.3276	0.6421	257	0.00020	5.371	436.1	96.550	1.849	425.0
4000.00	.04	573	2993.8	12.482	1.3321	0.6200	198	0.00016	5.930	441.4	159.707	1.879	432.0
$R = 0.800$; PERCENT FUEL = 13.60; O/F = 6.349													
1.00	150.00	3304	4586.9	13.622	1.2083	0.8231	851	0.00088	0.000	0.000	0.000	0.000	0.0
1.05	142.86	3277	4663.5	13.622	1.2086	0.8202	847	0.00088	0.285	505.8	2.172	0.203	45.1
1.20	125.00	3202	4500.4	13.622	1.2075	0.8189	837	0.00086	0.554	521.0	1.262	0.390	86.8
1.40	107.14	3118	4429.3	13.622	1.2084	0.8155	825	0.00085	0.757	466.1	1.062	0.526	117.1
1.60	93.75	3047	4369.2	13.622	1.2093	0.8123	815	0.00084	0.900	478.2	1.010	0.618	137.6
1.78	84.26	2992	4322.6	13.622	1.2101	0.8093	807	0.00083	1.000	476.9	1.000	0.681	151.6
2.00	75.00	2952	4271.9	13.622	1.2109	0.8074	798	0.00081	1.103	477.9	1.009	0.743	165.5
4.00	37.50	2595	3992.0	13.622	1.2160	0.8192	745	0.00075	1.606	499.8	1.301	1.021	227.4
10.00	15.00	2198	3672.1	13.622	1.2292	0.7252	673	0.00065	2.155	331.5	2.222	1.266	284.0
10.21	14.70	2190	3600.5	13.622	1.2290	0.7191	671	0.00065	2.168	332.1	2.251	1.271	285.0
20.00	7.50	1931	3496.5	13.622	1.2340	0.7094	617	0.00059	2.241	351.7	3.222	1.403	314.5
40.00	3.75	1690	3218.6	13.622	1.2441	0.7430	559	0.00052	2.918	368.8	5.710	1.513	337.0
100.00	1.50	1405	3075.1	13.622	1.2601	0.7088	483	0.00043	3.421	387.3	11.042	1.628	362.7
200.00	.75	1214	2944.8	13.622	1.2734	0.6782	425	0.00037	3.817	398.6	18.300	1.698	376.2
400.00	.38	1043	2828.9	13.622	1.2800	0.6210	370	0.00031	4.234	408.0	30.597	1.756	391.1
1000.00	.15	845	2705.0	13.622	1.3080	0.6195	302	0.00024	4.854	416.1	59.468	1.818	404.9
2000.00	.08	716	2624.5	13.622	1.3214	0.5996	255	0.00020	5.334	424.2	98.706	1.855	413.2
4000.00	.04	603	2557.7	13.622	1.3327	0.5844	214	0.00016	5.882	429.5	162.555	1.887	420.2
$R = 0.900$; PERCENT FUEL = 12.28; O/F = 7.143													
1.00	150.00	3336	4142.9	14.653	1.2044	0.7790	870	0.00084	0.000	0.000	0.000	0.000	0.0
1.05	142.86	3308	4121.0	14.653	1.2047	0.7781	866	0.00084	0.285	490.1	2.171	0.203	45.7
1.20	125.00	3234	4051.7	14.653	1.2055	0.7755	855	0.00083	0.554	511.0	1.262	0.389	84.1
1.40	107.14	3150	3955.0	14.653	1.2065	0.7723	843	0.00081	0.758	477.3	1.062	0.525	115.5
1.60	93.75	3078	3938.0	14.653	1.2073	0.7696	832	0.00080	0.900	469.6	1.009	0.618	133.3
1.78	84.42	3024	3895.2	14.653	1.2081	0.7674	824	0.00079	1.000	468.3	1.000	0.680	146.8
2.00	75.00	2962	3847.2	14.653	1.2089	0.7648	815	0.00078	1.104	469.4	1.009	0.744	160.4
4.00	37.50	2625	3584.9	14.653	1.2143	0.7684	761	0.00071	1.601	290.6	1.302	1.021	220.4
10.00	15.00	2227	3284.0	14.653	1.2230	0.7456	689	0.00065	2.157	321.5	2.226	1.266	273.4
10.21	14.70	2211	3277.0	14.653	1.2234	0.7452	687	0.00065	2.160	322.1	2.250	1.271	274.4
20.00	7.50	1959	3087.4	14.653	1.2231	0.7227	634	0.00056	2.241	341.4	3.653	1.404	303.1
40.00	3.75	1716	2914.8	14.653	1.2408	0.6980	575	0.00050	2.910	357.9	5.714	1.514	326.7
100.00	1.50	1431	2719.7	14.653	1.2604	0.6620	496	0.00042	3.417	372.4	11.109	1.620	

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P	Static pressure, P _s in lbs/in ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/g·°K*	Viscosity, μ, micro poises	Thermal conductivity, k, cal/sec·°K/cm*	Mach number, M	Specific impulse in vacuum, I _{vac} , sec	Area ratio, ε	Thrust coefficient, C _r	Specific impulse, I, sec
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	150.00	3341	3777.9	15.586	1.2057	0.7539	882	0.00001	0.000				
1.05	142.86	3315	3757.2	15.586	1.2056	0.7520	878	0.00001	0.000				
1.20	125.00	3259	3701.4	15.586	1.2040	0.7502	868	0.00079	554	30.0	2.170	0.202	42.4
1.40	107.14	3155	3636.6	15.586	1.2026	0.7477	852	0.00078	758	20.9	1.201	0.189	41.6
1.60	93.75	3084	3585.5	15.586	1.2004	0.7452	845	0.00076	901	16.0	1.062	0.173	41.0
1.78	84.45	3029	3546.7	15.586	1.2017	0.7432	836	0.00075	1.000	12.6	1.009	0.167	42.9
2.00	75.00	2968	3499.4	15.586	1.2019	0.7407	827	0.00074	1.104	16.1	1.009	0.164	44.4
4.00	37.50	2631	3252.2	15.586	1.2132	0.7254	772	0.00068	1.667	48.1	1.303	1.021	43.9
10.00	15.00	2234	2968.5	15.586	1.2217	0.705	699	0.00060	2.157	51.0	2.228	1.266	265.4
10.21	14.70	2226	2962.7	15.586	1.2219	0.7019	697	0.00060	2.168	51.7	2.254	1.271	266.3
20.00	7.50	1967	2783.1	15.586	1.2226	0.6828	642	0.00054	2.540	331.3	3.539	1.404	254.2
4.00	3.75	1724	2620.1	15.586	1.2274	0.6005	584	0.00048	2.915	347.0	3.792	1.015	317.4
100.00	1.50	1439	2435.8	15.586	1.2453	0.5259	207	0.00040	3.416	365.1	11.143	1.631	341.7
200.00	.75	1246	2317.3	15.586	1.2615	0.6041	450	0.00034	3.808	375.9	16.509	1.701	356.5
400.00	.38	1074	2219.4	15.586	1.2820	0.5796	394	0.00029	4.221	384.9	30.521	1.760	368.8
1000.00	.15	875	2101.5	15.586	1.3015	0.5907	324	0.00023	4.612	374.6	60.495	1.842	381.9
2000.00	.08	741	2030.3	15.586	1.3150	0.5522	276	0.00019	5.303	400.5	100.644	1.861	390.0
4000.00	.04	626	1970.0	15.586	1.3271	0.5173	232	0.00010	5.841	405.4	167.211	1.893	396.6
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	150.00	3219	2626.1	19.176	1.2047	0.6098	905	0.00067	0.000				
1.05	142.86	3193	2609.9	19.176	1.2020	0.6091	901	0.00067	.285	420.8	2.171	0.203	37.6
1.20	125.00	3121	2566.2	19.176	1.2058	0.6071	890	0.00066	.554	267.1	1.282	0.389	72.2
1.40	107.14	3040	2517.0	19.176	1.2068	0.6047	876	0.00064	.758	238.1	1.002	0.526	97.4
1.60	93.75	2971	2475.4	19.176	1.2077	0.6026	865	0.00063	.900	231.5	1.010	0.610	114.5
1.78	84.41	2911	2442.6	19.176	1.2094	0.6008	856	0.00063	1.000	230.4	1.000	0.680	126.1
2.00	75.00	2859	2408.0	19.176	1.2093	0.5988	846	0.00062	1.103	231.3	1.009	0.743	137.7
4.00	37.50	2531	2214.6	19.176	1.2147	0.5882	787	0.00056	1.607	249.6	1.302	1.021	189.2
10.00	15.00	2148	1992.0	19.176	1.2255	0.5014	710	0.00049	2.157	276.0	2.225	1.266	234.7
10.21	14.70	2140	1988.2	19.176	1.2251	0.5009	708	0.00049	2.168	276.2	2.255	1.271	235.6
20.00	7.50	1889	1847.9	19.176	1.2314	0.5015	651	0.00044	2.541	292.9	3.531	1.404	260.2
4.00	3.75	1655	1720.8	19.176	1.2408	0.5340	592	0.00039	2.917	307.2	5.736	1.514	280.7
100.00	1.50	1380	1577.0	19.176	1.2557	0.5089	515	0.00033	3.419	322.7	11.104	1.630	302.1
200.00	.75	1195	1484.7	19.176	1.2684	0.4989	458	0.00028	3.813	322.2	18.438	1.700	315.1
400.00	.38	1029	1404.9	19.176	1.2823	0.4708	403	0.00024	4.227	340.2	30.698	1.758	326.0
1000.00	.15	837	1316.6	19.176	1.3007	0.4482	354	0.00019	4.819	348.7	60.267	1.821	337.5
2000.00	.08	711	1261.1	19.176	1.3141	0.4356	287	0.00016	5.311	353.9	100.322	1.859	344.6
4000.00	.04	601	1214.1	19.176	1.3263	0.4121	244	0.00013	5.848	358.2	166.710	1.891	350.5
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	150.00	3045	2016.0	21.610	1.2087	0.5325	900	0.00058	0.000				
1.05	142.86	3020	2002.4	21.610	1.2091	0.5318	898	0.00058	.285	385.5	2.173	0.203	39.4
1.20	125.00	2951	1965.8	21.610	1.2100	0.5299	884	0.00057	.553	244.6	1.263	0.390	66.1
1.40	107.14	2873	1924.5	21.610	1.2111	0.5275	870	0.00056	.756	218.0	1.053	0.528	89.2
1.60	93.75	2806	1889.6	21.610	1.2121	0.5255	858	0.00055	.959	211.9	1.010	0.618	104.9
1.78	84.41	2755	1862.4	21.610	1.2129	0.5238	848	0.00054	1.000	210.9	1.000	0.682	115.6
2.00	75.00	2699	1835.2	21.610	1.2139	0.5220	838	0.00053	1.102	211.7	1.009	0.744	126.1
4.00	37.50	2389	1671.3	21.610	1.2196	0.5106	777	0.00049	1.605	226.3	1.294	1.021	173.2
10.00	15.00	2017	1486.2	21.610	1.2289	0.4937	697	0.00042	2.156	252.3	2.215	1.266	214.7
10.21	14.70	2009	1482.4	21.610	1.2291	0.4933	695	0.00042	2.168	252.8	2.244	1.270	215.5
20.00	7.50	1769	1365.7	21.610	1.2374	0.4793	537	0.00038	2.542	267.6	3.508	1.402	257.9
4.00	3.75	1546	1260.1	21.610	1.2470	0.4645	577	0.00033	2.921	280.6	5.065	1.514	290.5
100.00	1.50	1264	1141.2	21.610	1.2619	0.4430	504	0.00028	3.427	294.5	10.974	1.626	275.9
200.00	.75	1109	1065.1	21.610	1.2746	0.4289	445	0.00024	3.826	303.1	18.178	1.696	287.7
400.00	.38	992	999.5	21.610	1.2878	0.4114	352	0.00021	4.246	310.2	30.200	1.753	297.4
1000.00	.15	772	927.1	21.610	1.3057	0.3927	326	0.00017	4.847	317.9	59.146	1.813	307.8
2000.00	.08	655	881.7	21.610	1.3157	0.3805	281	0.00014	5.346	322.5	98.462	1.852	314.2
4000.00	.04	552	843.3	21.610	1.3307	0.3700	240	0.00012	5.891	326.4	163.108	1.889	319.4
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	150.00	2695	1361.4	24.614	1.2194	0.4488	859	0.00047	0.000				
1.05	142.86	2672	1408.4	24.614	1.2190	0.4481	855	0.00047	.283	359.8	2.180	0.203	30.3
1.20	125.00	2608	1342.4	24.614	1.2209	0.4463	844	0.00046	.551	215.5	1.266	0.391	58.3
1.40	107.14	2536	1310.4	24.614	1.2221	0.4442	829	0.00045	.754	191.9	1.064	0.527	76.0
1.60	93.75	2475	1285.3	24.614	1.2233	0.4423	812	0.00044	.956	186.5	1.010	0.620	94.4
1.78	83.95	2420	1261.5	24.614	1.2243	0.4401	803	0.00044	1.000	185.6	1.000	0.685	102.1
2.00	75.00	2376	1239.7	24.614	1.2223	0.4391	792	0.00043	1.098	186.2	1.008	0.745	111.1
4.00	37.50	2089	1114.9	24.614	1.2352	0.4265	731	0.00039	1.602	200.5	1.293	1.022	152.3
10.00	15.00	1752	973.1	24.614	1.2427	0.4134	649	0.00033	2.155	241.1	2.192	1.265	188.3
10.21	14.70	1745	970.2	24.614	1.2420	0.4130	647	0.00033	2.167	241.6	2.219	1.269	189.2
20.00	7.50	1527	881.5	24.614	1.2518	0.4014	585	0.00032	2.545	249.3	3.451	1.339	208.6
4.00	3.75	1326	801.7	24.614	1.2621	0.3881	520	0.00026	2.930	240.3	5.563	1.507	224.6
100.00	1.50	1071	714.6	24.614	1.2713	0.4710	457	0.00022	3.448	257.1	10.639	1.610	241.2
200.00	.75	936	652.4	24.614	1.2807	0.4594	403	0.00019	3.808	264.3	17.563	1.656	251.3
400.00	.38	799	607.4	24.614	1.2926	0.4374	350	0.00016	4.291	270.0	29.027	1.741</	

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSUMED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P ₀	Static pressure, P, lb/sq in abs	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M _w	Isentropic exponent, γ	Specific heat, c _p , cal/deg K	Viscosity, μ, lb sec/ft ²	Thermal conductivity, k, cal/sec/in ² K	Mach number, M	Specific impulse in vacuum, I _{sp} , sec	Area ratio, ε	Thrust coefficient, C _t	Specific impulse, I, lb sec/lb
<i>R = 4.000; PERCENT FUEL = 5.054; O/F = 31.745</i>													
1.00	150.00	2363	1054.4	26.287	1.2315	0.4022	604	0.0000	0.000	0.000	2.157	0.300	0.0
1.05	142.86	2291	1049.7	26.287	1.2314	0.4019	797	0.0000	0.262	507.7	2.157	0.294	27.1
1.10	129.00	2203	1044.4	26.287	1.2312	0.4017	764	0.0000	0.298	495.0	2.157	0.294	26.8
1.15	117.14	2117	1039.2	26.287	1.2308	0.4016	730	0.0000	0.309	483.6	2.157	0.294	21.1
1.20	99.75	2101	1034.1	26.287	1.2301	0.4007	757	0.0000	0.302	466.0	2.011	0.291	89.6
1.25	93.50	2114	1029.9	26.287	1.2295	0.4004	746	0.0000	0.307	467.7	1.930	0.299	92.7
1.30	79.00	2074	1025.4	26.287	1.2289	0.4001	750	0.0000	0.304	466.3	1.808	0.297	120.5
1.35	71.50	1989	1020.9	26.287	1.2281	0.4001	763	0.0000	0.302	459.0	1.728	0.295	137.6
1.40	65.00	1903	1016.4	26.287	1.2276	0.4001	751	0.0000	0.295	445.5	1.656	0.293	170.6
1.45	59.75	1818	1011.9	26.287	1.2270	0.4001	767	0.0000	0.286	439.0	1.592	0.288	170.6
1.50	55.00	1733	1007.5	26.287	1.2264	0.4001	753	0.0000	0.274	429.4	1.539	0.286	167.3
1.55	50.75	1648	1003.0	26.287	1.2258	0.4001	760	0.0000	0.264	419.6	1.493	0.281	164.0
1.60	47.50	1563	998.5	26.287	1.2251	0.4001	757	0.0000	0.254	409.8	1.456	0.278	161.7
1.65	44.50	1478	994.0	26.287	1.2244	0.4001	764	0.0000	0.244	399.9	1.424	0.275	159.4
1.70	41.75	1393	989.5	26.287	1.2237	0.4001	760	0.0000	0.234	389.9	1.394	0.272	157.1
1.75	39.25	1308	985.0	26.287	1.2230	0.4001	758	0.0000	0.224	379.9	1.364	0.269	154.8
1.80	36.90	1223	979.5	26.287	1.2223	0.4001	765	0.0000	0.214	369.9	1.334	0.266	152.5
1.85	34.75	1138	975.0	26.287	1.2216	0.4001	752	0.0000	0.204	359.9	1.304	0.263	150.2
1.90	32.75	1053	969.5	26.287	1.2209	0.4001	759	0.0000	0.194	349.9	1.274	0.260	147.9
1.95	30.90	968	965.0	26.287	1.2201	0.4001	755	0.0000	0.184	339.9	1.244	0.257	145.6
2.00	29.25	883	959.5	26.287	1.2194	0.4001	762	0.0000	0.174	329.9	1.214	0.254	143.3
2.05	27.75	798	955.0	26.287	1.2187	0.4001	758	0.0000	0.164	319.9	1.184	0.251	141.0
2.10	26.40	713	949.5	26.287	1.2180	0.4001	765	0.0000	0.154	309.9	1.154	0.248	138.7
2.15	25.20	628	944.0	26.287	1.2173	0.4001	751	0.0000	0.144	299.9	1.124	0.245	136.4
2.20	24.15	543	938.5	26.287	1.2166	0.4001	758	0.0000	0.134	289.9	1.094	0.242	134.1
2.25	23.20	458	933.0	26.287	1.2159	0.4001	765	0.0000	0.124	279.9	1.064	0.239	131.8
2.30	22.35	373	927.5	26.287	1.2152	0.4001	751	0.0000	0.114	269.9	1.034	0.236	129.5
2.35	21.60	288	922.0	26.287	1.2145	0.4001	758	0.0000	0.104	259.9	1.004	0.233	127.2
2.40	20.95	203	916.5	26.287	1.2138	0.4001	765	0.0000	0.094	249.9	9.744	0.230	124.9
2.45	20.40	118	911.0	26.287	1.2131	0.4001	751	0.0000	0.084	239.9	9.444	0.227	122.6
2.50	19.90	33	905.5	26.287	1.2124	0.4001	758	0.0000	0.074	229.9	9.144	0.224	120.3
2.55	19.45	-	900.0	26.287	1.2117	0.4001	765	0.0000	0.064	219.9	8.844	0.221	118.0
2.60	19.00	-	894.5	26.287	1.2110	0.4001	751	0.0000	0.054	209.9	8.544	0.218	115.7
2.65	18.60	-	889.0	26.287	1.2103	0.4001	758	0.0000	0.044	199.9	8.244	0.215	113.4
2.70	18.25	-	883.5	26.287	1.2096	0.4001	765	0.0000	0.034	189.9	7.944	0.212	111.1
2.75	17.90	-	878.0	26.287	1.2089	0.4001	751	0.0000	0.024	179.9	7.644	0.209	108.8
2.80	17.55	-	872.5	26.287	1.2082	0.4001	758	0.0000	0.014	169.9	7.344	0.206	106.5
2.85	17.20	-	867.0	26.287	1.2075	0.4001	765	0.0000	0.004	159.9	7.044	0.203	104.2
2.90	16.85	-	861.5	26.287	1.2068	0.4001	751	0.0000	-	149.9	6.744	0.200	101.9
2.95	16.50	-	856.0	26.287	1.2061	0.4001	758	0.0000	-	139.9	6.444	0.197	99.6
3.00	16.15	-	850.5	26.287	1.2054	0.4001	765	0.0000	-	129.9	6.144	0.194	97.3
3.05	15.80	-	845.0	26.287	1.2047	0.4001	751	0.0000	-	119.9	5.844	0.191	95.0
3.10	15.45	-	839.5	26.287	1.2040	0.4001	758	0.0000	-	109.9	5.544	0.188	92.7
3.15	15.10	-	834.0	26.287	1.2033	0.4001	765	0.0000	-	99.9	5.244	0.185	90.4
3.20	14.75	-	828.5	26.287	1.2026	0.4001	751	0.0000	-	89.9	4.944	0.182	88.1
3.25	14.40	-	823.0	26.287	1.2019	0.4001	758	0.0000	-	79.9	4.644	0.179	85.8
3.30	14.05	-	817.5	26.287	1.2012	0.4001	765	0.0000	-	69.9	4.344	0.176	83.5
3.35	13.70	-	812.0	26.287	1.2005	0.4001	751	0.0000	-	59.9	4.044	0.173	81.2
3.40	13.35	-	806.5	26.287	1.1998	0.4001	758	0.0000	-	49.9	3.744	0.170	78.9
3.45	13.00	-	801.0	26.287	1.1991	0.4001	765	0.0000	-	39.9	3.444	0.167	76.6
3.50	12.65	-	995.5	26.287	1.1984	0.4001	751	0.0000	-	29.9	3.144	0.164	74.3
3.55	12.30	-	990.0	26.287	1.1977	0.4001	758	0.0000	-	19.9	2.844	0.161	72.0
3.60	11.95	-	984.5	26.287	1.1970	0.4001	765	0.0000	-	9.9	2.544	0.158	69.7
3.65	11.60	-	979.0	26.287	1.1963	0.4001	751	0.0000	-	-	2.544	0.155	67.4
3.70	11.25	-	973.5	26.287	1.1956	0.4001	758	0.0000	-	-	-	0.152	65.1
3.75	10.90	-	968.0	26.287	1.1949	0.4001	765	0.0000	-	-	-	-	62.8
3.80	10.55	-	962.5	26.287	1.1942	0.4001	751	0.0000	-	-	-	-	60.5
3.85	10.20	-	957.0	26.287	1.1935	0.4001	758	0.0000	-	-	-	-	58.2
3.90	9.85	-	951.5	26.287	1.1928	0.4001	765	0.0000	-	-	-	-	55.9
3.95	9.50	-	946.0	26.287	1.1921	0.4001	751	0.0000	-	-	-	-	53.6
4.00	9.15	-	940.5	26.287	1.1914	0.4001	758	0.0000	-	-	-	-	51.3
4.05	8.80	-	935.0	26.287	1.1907	0.4001	765	0.0000	-	-	-	-	49.0
4.10	8.45	-	929.5	26.287	1.1899	0.4001	751	0.0000	-	-	-	-	46.7
4.15	8.10	-	924.0	26.287	1.1892	0.4001	758	0.0000	-	-	-	-	44.4
4.20	7.75	-	918.5	26.287	1.1885	0.4001	765	0.0000	-	-	-	-	42.1
4.25	7.40	-	913.0	26.287	1.1878	0.4001	751	0.0000	-	-	-	-	39.8
4.30	7.05	-	907.5	26.287	1.1871	0.4001	758	0.0000	-	-	-	-	37.5
4.35	6.70	-	902.0	26.287	1.1864	0.4001	765	0.0000	-	-	-	-	35.2
4.40	6.35	-	896.5	26.287	1.1857	0.4001	751	0.0000	-	-	-	-	32.9
4.45	6.00	-	891.0	26.287	1.1850	0.4001	758	0.0000	-	-	-	-	30.6
4.50	5.65	-	885.5	26.287	1.1843	0.4001	765	0.0000	-	-	-	-	28.3
4.55	5.30	-	880.0	26.287	1.1836	0.4001	751	0.0000	-	-	-	-	26.0
4.60	4.95	-	874.5	26.287	1.1829	0.4001	758	0.0000	-	-	-	-	23.7
4.65	4.60	-	869.0	26.287	1.1822	0.4001	765	0.0000	-	-	-	-	21.4
4.70	4.25	-	863.5	26.287	1.1815	0.4001	751	0.0000	-	-	-	-	19.1
4.75	3.90	-	858.0	26.287	1.1808	0.4001	758	0.0000	-	-	-	-	16.8
4.80	3.55	-	852.5	26.287	1.1801	0.4001	765	0.0000	-	-	-	-	14.5
4.85	3.20	-	847.0	26.287	1.1								

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _{c/P}	Static pressure, P _s , lb/in ² abs	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c _p , cal/g·K ^o	Viscosity, μ, poises	Thermal conductivity, k, cal/sec ^o ·cm ^o	Mach number, M	Specific impulse in vacuum, I _{vac} , sec	Area ratio, ε	Thrust coefficient, C _t	Specific impulse, I, lb-sec/lb
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	300.00	1183	5314.5	4.416	1.3396	1.7773	314	0.00073	0.000			0.000	0.0
1.05	285.71	1168	5281.7	4.416	1.3406	1.7710	311	0.00073	.471	330.0	2.420	.210	47.4
1.20	250.00	1129	5210.6	4.416	1.3436	1.7597	305	0.00070	.527	334.2	1.297	.403	90.8
1.40	214.29	1065	5141.8	4.416	1.3459	1.7472	293	0.00066	.722	296.1	1.061	.543	142.2
1.60	187.50	1049	5071.7	4.416	1.3479	1.7309	285	0.00066	.860	268.6	1.018	.636	145.2
1.87	160.00	1008	5000.8	4.416	1.3528	1.7257	276	0.00063	1.000	284.1	1.000	.725	163.4
2.00	150.00	989	4975.4	4.416	1.3549	1.7210	272	0.00062	1.059	284.4	1.003	.761	171.5
4.00	75.00	824	4699.4	4.416	1.3621	1.6862	254	0.0002	1.066	301.7	1.233	1.031	232.3
10.00	30.00	642	4332.5	4.416	1.3748	1.6702	180	0.00042	2.152	327.5	1.974	1.257	453.1
20.00	15.00	532	4078.8	4.416	1.3794	1.6594	159	0.00035	2.968	343.5	2.982	1.376	329.9
20.41	14.70	529	4040.9	4.416	1.3801	1.6590	158	0.00035	2.959	343.9	3.020	1.379	310.6
40.00	7.50	439	4026.9	4.416	1.3824	1.6289	133	0.00029	3.031	356.4	4.620	1.467	330.4
100.00	3.00	340	3699.0	4.416	1.3862	1.6073	104	0.00023	3.048	369.8	6.432	1.558	350.8
200.00	1.50	280	3602.6	4.416	1.3926	1.5901	82	0.00018	4.149	377.7	13.431	1.610	362.0
400.00	.75	230	3723.2	4.416	1.4008	1.5502	70	0.00015	4.675	384.1	21.488	1.652	372.0
1000.00	.38	175	3840.1	4.416	1.4139	1.4867	55	0.00011	5.448	390.6	39.928	1.694	381.6
2000.00	.19	142	3590.9	4.416	1.4250	1.4389	43	0.00009	6.076	394.3	63.572	1.719	387.2
4000.00	.08	114	3551.2	4.416	1.4275	1.4055	36	0.00007	6.845	397.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	300.00	1514	2969.7	5.216	1.3079	1.6183	402	0.00084	0.000			0.000	0.0
1.05	285.71	1497	2941.7	5.216	1.3070	1.6180	399	0.00083	.274	326.2	2.235	.209	49.3
1.20	250.00	1450	2866.8	5.216	1.3100	1.6062	389	0.00081	.253	348.6	1.269	.400	94.6
1.40	214.29	1390	2783.2	5.216	1.3129	1.5867	378	0.00078	.730	309.3	1.077	.539	127.4
1.60	187.50	1334	2713.2	5.216	1.3189	1.5772	369	0.00076	.869	299.6	1.016	.632	149.4
1.87	162.44	1307	2640.5	5.216	1.3211	1.5521	359	0.00073	1.000	297.3	1.000	.716	169.2
2.00	150.00	1262	2601.1	5.216	1.3235	1.5294	353	0.00072	1.058	297.8	1.004	.757	179.1
4.00	75.00	1079	2290.0	5.216	1.3391	1.5046	207	0.00061	1.272	316.7	1.244	1.029	243.2
10.00	30.00	852	1954.3	5.216	1.3528	1.4516	651	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	15.00	709	1748.8	5.216	1.3626	1.4323	213	0.00040	2.713	356.0	3.049	1.379	325.9
20.41	14.70	705	1743.3	5.216	1.3628	1.4222	212	0.00040	2.786	352.4	3.088	1.382	326.7
40.00	7.50	568	1578.0	5.216	1.3719	1.4050	179	0.00034	3.010	376.0	4.739	1.472	346.0
100.00	.50	458	1596.3	5.216	1.3811	1.3713	142	0.00026	2.619	376.2	8.679	1.562	370.0
200.00	.19	379	1686.2	5.216	1.3801	1.3607	117	0.00022	4.111	399.1	12.570	1.619	384.7
400.00	.08	312	1195.2	5.216	1.3801	1.3607	96	0.00018	4.635	408.1	22.496	1.662	394.9
1000.00	.30	242	1097.0	5.216	1.3913	1.3490	74	0.00013	5.394	415.4	41.919	1.706	405.5
2000.00	.15	198	1041.1	5.216	1.3916	1.3277	61	0.00011	6.014	417.7	67.567	1.733	409.5
4000.00	.08	161	993.4	5.216	1.3920	1.3268	50	0.00009	6.704	421.1	108.754	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	300.00	1817	1249.3	6.016	1.2835	1.4955	481	0.00092	0.000			0.000	0.0
1.05	285.71	1777	1220.2	6.016	1.2844	1.4917	477	0.00091	.276	563.4	2.219	.207	50.3
1.20	250.00	1742	1142.1	6.016	1.2870	1.4813	467	0.00089	.528	566.2	1.283	.398	96.6
1.40	214.29	1665	1058.8	6.016	1.2920	1.4693	458	0.00086	.726	516.2	1.073	.536	150.1
1.60	187.50	1632	981.5	6.016	1.2921	1.4591	446	0.00083	.876	506.6	1.015	.629	152.6
1.87	165.50	1586	907.4	6.016	1.2924	1.4440	436	0.00081	1.000	504.2	1.000	.708	171.8
2.00	150.00	1554	864.0	6.016	1.2973	1.4412	427	0.00080	1.076	502.1	1.003	.734	183.1
4.00	75.00	1324	555.2	6.016	1.3170	1.3513	378	0.00068	1.274	527.5	1.250	1.027	249.3
10.00	30.00	1057	176.3	6.016	1.3249	1.3227	314	0.00054	2.147	552.3	6.458	1.258	305.6
20.00	15.00	887	995.5	6.016	1.3401	1.2848	269	0.00046	2.626	573.6	9.127	1.382	332.7
20.41	14.70	882	994.5	6.016	1.3404	1.2850	261	0.00045	2.775	574.1	9.161	1.386	335.5
40.00	7.50	740	976.6	6.016	1.3509	1.2859	229	0.00030	2.987	588.6	4.583	1.476	359.0
100.00	.50	580	956.5	6.016	1.3635	1.2520	181	0.00020	3.281	404.1	8.985	1.572	382.3
200.00	.15	461	944.5	6.016	1.3717	1.2471	151	0.00012	4.084	415.3	18.579	1.630	395.9
20.41	.14.70	399	934.7	6.016	1.3722	1.2410	124	0.00012	4.782	420.9	23.427	1.672	406.6
1000.00	.30	310	9241.1	6.016	1.3841	1.1740	92	0.00012	5.327	428.7	42.070	1.744	418.0
2000.00	.15	256	9176.2	6.016	1.3869	1.1809	76	0.00012	5.749	433.2	11.474	1.744	424.7
4000.00	.08	210	9123.3	6.016	1.4019	1.1402	54	0.00010	6.066	437.1	115.539	1.771	430.1
R = 0.300, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	300.00	2093	5932.7	6.814	1.2647	1.3935	550	0.00097	0.000			0.000	0.0
1.05	285.71	2072	5905.1	6.814	1.2657	1.3905	547	0.00096	.274	585.2	2.205	.207	50.8
1.20	250.00	2015	5625.2	6.814	1.2676	1.3816	536	0.00094	.542	585.7	1.278	.396	97.0
1.40	214.29	1950	5734.4	6.814	1.2701	1.3713	529	0.00091	.741	514.7	1.071	.533	131.4
1.60	187.50	1899	5675.6	6.814	1.2742	1.3621	514	0.00089	.881	510.1	1.013	.626	154.6
1.87	165.50	1844	5590.0	6.814	1.2747	1.3532	503	0.00087	1.000	508.2	1.000	.701	172.1
2.00	150.00	1808	5537.4	6.814	1.2760	1.3405	497	0.00085	1.082	506.9	1.008	.751	189.1
4.00	75.00	1590	5400.7	6.814	1.2870	1.3170	444	0.00074	1.279	539.3	1.266	1.027	252.4
10.00	30.00	1225	5820.7	6.814	1.3112	1.2251	375	0.00060	2.146	581.5	2.084	1.260	310.2
20.00	15.00	1062	5934.0	6.814	1.3221	1.1667	329	0.00050	2.625	580.9	3.420	1.387	341.4
20.41	14.70	1037	5760.7	6.814	1.3222	1.1614	323	0.00050	2.657	581.4	3.424	1.390	342.2
40.00	7.50	873	5395.0	6.814	1.3300	1.1508	278	0.00042	2.969	586.7	5.035	1.462	365.7
1000.00	.30	736	5054.0	6.814	1.3570	1.0745	225	0.00035	2.924	435.2	1.052	.585	390.2
2000.00	.15	588	5056.5	6.814	1.3570	1.0507	186	0.00027	4.014	422.9	1.064	1.643	404.5
20.41	.14.70	487	5044.0	6.814	1.3605	1.0508	156	0.00023	4.928	430.9	24.219	1.689	416.0

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P ₀	Static pressure, P, lb./sq.in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, γ	Specific heat, c _p , cal/(g·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec·°K·cm)	Mach number, M	Specific impulse in vacuum, I _{sp} , sec.	Area ratio, ε	Thrust coefficient, C _r	Specific impulse, I, lb.(sec./lb)
<i>R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778</i>													
1.00	300.00	2344	8892.8	7.607	1.2502	610	0.00100	0.000	2.116	1.261	0.000	0.205	0.0
1.05	285.71	2321	8863.0	7.607	1.2509	607	0.00099	0.280	264.5	2.199	0.000	50.9	50.9
1.20	250.00	2259	8783.2	7.607	1.2527	607	0.00097	0.245	360.6	1.274	0.000	394	97.7
1.40	214.29	2190	8693.6	7.607	1.2546	605	0.00094	0.145	320.7	1.069	0.000	552	131.6
1.60	187.50	2131	8618.2	7.607	1.2567	607	0.00092	0.086	311.3	1.012	0.000	624	154.6
1.81	165.96	2079	8551.1	7.607	1.2584	605	0.00090	1.000	309.4	1.000	0.000	696	172.4
2.00	150.00	2036	8496.8	7.607	1.2600	607	0.00089	1.087	310.3	1.007	0.000	749	185.6
4.00	75.00	1760	8153.6	7.607	1.2717	603	0.00078	1.590	332.5	1.274	0.024	253.6	253.6
10.00	30.00	1440	7771.6	7.607	1.2896	432	0.00064	2.150	364.7	2.116	1.261	312.3	312.3
20.00	15.00	1229	7530.3	7.607	1.3046	378	0.00055	2.551	384.9	3.275	1.390	364.3	364.3
20.41	14.70	1223	7523.7	7.607	1.3030	377	0.00054	2.553	385.4	3.319	1.394	365.1	365.1
4.00	7.50	1042	7325.1	7.607	1.3199	377	0.00046	4.954	401.4	5.178	1.491	369.3	369.3
100.00	3.00	831	7101.8	7.607	1.3374	402	0.00036	3.014	418.7	9.654	1.054	394.8	394.8
200.00	1.50	696	6963.9	7.607	1.3482	414	0.00030	3.968	429.0	15.587	1.654	409.7	409.7
400.00	.75	581	6840.6	7.607	1.3560	3949	0.00023	4.457	437.4	25.280	1.703	421.7	421.7
1000.00	.30	466	6725.1	7.607	1.3639	3970	0.00019	5.168	446.2	48.144	1.756	434.3	434.3
2000.00	.15	378	6649.8	7.607	1.3690	3963	0.00015	5.758	451.5	78.603	1.784	441.8	441.8
4000.00	.08	314	6587.3	7.607	1.3740	3956	0.00012	6.400	459.8	128.518	1.808	447.9	447.9
<i>R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175</i>													
1.00	300.00	2565	8050.5	8.389	1.2389	662	0.00101	0.000	2.192	0.205	0.000	0.0	0.0
1.05	285.71	2541	8021.0	8.389	1.2394	662	0.00100	.281	367.5	1.271	0.393	97.3	97.3
1.20	250.00	2476	7941.7	8.389	1.2409	660	0.00098	.547	359.5	1.067	0.530	131.2	131.2
1.40	214.29	2403	7825.6	8.389	1.2427	658	0.00096	.748	319.9	1.012	0.622	154.1	154.1
1.60	187.50	2381	7777.6	8.389	1.2444	656	0.00094	.889	310.6	1.000	0.692	171.4	171.4
1.80	166.67	2267	7713.0	8.389	1.2479	653	0.00092	1.000	308.9	1.007	0.748	185.2	185.2
2.00	150.00	2240	7656.5	8.389	1.2473	651	0.00091	1.091	309.8	1.023	0.781	199.0	199.0
4.00	75.00	1948	7313.1	8.389	1.2571	555	0.00081	1.594	332.6	1.281	1.023	253.3	253.3
10.00	30.00	1608	6928.0	8.389	1.2730	482	0.00068	2.152	365.6	2.142	1.262	312.5	312.5
20.00	15.00	1382	6682.9	8.389	1.2870	487	0.00058	2.548	386.3	3.335	1.393	345.0	345.0
20.41	14.70	1376	6676.2	8.389	1.2874	461	0.00058	2.560	386.8	3.380	1.397	345.8	345.8
4.00	7.50	1180	6472.9	8.389	1.3020	373	0.00049	2.944	403.3	5.305	1.496	370.5	370.5
100.00	3.00	949	6242.4	8.389	1.3115	378	0.00039	3.488	421.3	9.963	1.002	396.6	396.6
200.00	1.50	800	6099.1	8.389	1.3193	395	0.00032	3.929	432.1	16.102	1.664	412.1	412.1
400.00	.75	671	5978.6	8.389	1.3446	391	0.00027	4.403	440.9	26.111	1.715	424.6	424.6
1000.00	.30	529	5849.0	8.389	1.3570	3931	0.00021	5.091	450.1	50.311	1.768	437.7	437.7
2000.00	.15	441	5769.6	8.389	1.3612	3926	0.00017	5.667	459.7	82.327	1.759	445.5	445.5
4000.00	.08	366	5703.5	8.389	1.3663	3916	0.00014	6.293	460.3	134.916	1.825	451.9	451.9
<i>R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571</i>													
1.00	300.00	2755	7354.5	9.152	1.2300	1.1611	705	0.00101	0.000	2.186	0.204	50.3	50.3
1.05	285.71	2730	7325.4	9.152	1.2303	1.1591	701	0.00100	.282	563.2	1.268	0.392	96.6
1.20	250.00	2662	7247.2	9.152	1.2318	1.1537	691	0.00098	.549	357.0	1.067	0.529	130.3
1.40	214.29	2596	7159.4	9.152	1.2334	1.1475	679	0.00096	.751	317.8	1.066	0.529	130.3
1.60	187.50	2521	7085.4	9.152	1.2348	1.1420	669	0.00094	.892	308.7	1.011	0.621	153.0
1.79	167.23	2467	7023.4	9.152	1.2360	1.1372	661	0.00093	1.000	307.0	1.000	0.689	169.7
2.00	150.00	2416	6965.8	9.152	1.2374	1.1324	652	0.00092	1.094	304.0	1.008	0.747	183.9
4.00	75.00	2112	6625.4	9.152	1.2459	1.1000	599	0.00082	1.598	331.1	1.280	1.022	251.9
10.00	30.00	1755	6241.6	9.152	1.2600	1.0523	576	0.00070	2.153	364.5	2.163	1.263	311.2
20.00	15.00	1517	5995.6	9.152	1.2748	1.0150	471	0.00060	2.546	385.5	3.304	1.396	345.9
20.41	14.70	1511	5980.4	9.152	1.2750	1.0126	469	0.00060	2.558	386.1	3.431	1.399	344.7
4.00	7.50	1304	5783.6	9.152	1.2868	0.9743	415	0.00052	2.936	403.0	5.411	1.501	369.7
1000.00	3.00	1057	5549.4	9.152	1.3067	.9251	.544	0.00041	3.469	421.5	10.232	1.609	396.3
2000.00	1.50	960	5242.0	9.152	1.3208	.8539	.295	0.00034	3.898	432.7	16.676	1.673	412.1
4000.00	.75	755	5278.6	9.152	1.3334	.6684	.249	0.00028	4.357	441.8	27.260	1.725	425.0
1000.00	.30	599	5144.5	9.152	1.3482	.8443	.197	0.00022	5.026	451.4	52.343	1.780	438.5
2000.00	.15	500	5062.0	9.152	1.3533	.8300	.164	0.00018	5.584	457.2	85.868	1.813	446.6
4000.00	.08	417	4993.4	9.152	1.3590	.8201	.134	0.00017	6.196	464.0	141.008	1.840	453.3
<i>R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968</i>													
1.00	300.00	2915	6769.6	9.891	1.2220	1.1020	741	0.00100	0.000	2.182	0.204	49.8	49.8
1.05	285.71	2809	6741.2	9.891	1.2224	1.1002	737	0.00100	.280	557.3	1.267	0.391	95.6
1.20	250.00	2619	6604.6	9.891	1.2240	1.0723	727	0.00100	.554	353.4	1.065	0.528	129.0
1.40	214.29	2747	6570.5	9.891	1.2261	1.0686	715	0.00100	.754	314.7	1.011	0.620	151.5
1.60	187.50	2674	6509.4	9.891	1.2273	1.0646	702	0.00100	.894	305.8	1.000	0.687	167.7
1.79	167.67	2619	6444.5	9.891	1.2284	1.0604	697	0.00100	1.000	304.2	1.008	0.746	182.1
2.00	150.00	2569	6388.5	9.891	1.2295	1.0623	689	0.00100	1.097	305.2	1.088	0.746	199.6
4.00	75.00	2250	6053.6	9.891	1.2372	1.0478	636	0.00083	1.600	326.4	1.290	1.022	249.6
10.00	30.00	1881	5674.2	9.891	1.2497	1.0055	564	0.00071	2.154	362.0	2.180	1.264	308.7
20.00	15.00	1653	5424.0	9.891	1.2611	.9702	.508	0.00062	2.545	383.3	3.424	1.398	341.4
20.41	14.70	1627	5423.1	9.891	1.2612	.9692	.500	0.00062	2.556	383.8	3.471	1.401	342.3
4.00	7.50	1411	5210.1	9.891	1.2744	.9351	.451	0.00053	2.951	401.0	5.497	1.504	367.4
1000.00	3.00	1124	4792.7	9.891	1.2870	.8648	.376	0.00043	3.474	419.9	10.428	1.614	394.3
2000.00	1.50	961	4634.4	9.891	1.3007	.8510	.326	0.00030	3.673	431.3	17.118	1.680	410.4
4000.00	.75	631	4703.4	9.891	1.3223	.8242	.277	0.					

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s , lb/sq in abs	Temperature, T_s , °K	Enthalpy, h_s , cal/g	Molecular weight, \bar{m}	Isentropic exponent, γ	Specific heat, c_p , cal/(lb·°R)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/sec·°R/cm	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/sec/lb	Area ratio, E	Thrust coefficient, C_f , lb/sec/lb	Specific impulse, I , lb/sec/lb
$R = 0.600$, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	300.00	3155	5841.6	11.290	1.2131	1.0021	.796	0.00097	0.000	542.6	1.170	0.000	0.0
1.05	285.71	3128	5614.6	11.290	1.2134	1.0008	.795	0.00097	.284	542.6	1.170	.203	45.4
1.20	250.00	3027	5742.0	11.290	1.2144	.9970	.783	0.00095	.552	344.4	1.254	.390	95.1
1.40	214.29	2973	5660.4	11.290	1.2126	.9924	.771	0.00093	.755	309.6	1.063	.267	125.6
1.60	187.50	2903	5591.2	11.290	1.2107	.9883	.761	0.00092	.898	294.2	1.010	.019	147.6
1.78	168.29	2848	5550.4	11.290	1.2106	.9849	.753	0.00091	1.000	296.6	1.000	.083	164.9
2.00	150.00	2790	5479.4	11.290	1.2106	.9813	.744	0.00089	1.100	297.3	1.004	.744	177.5
4.00	75.00	2660	5159.5	11.290	1.2249	.9589	.692	0.00082	1.604	320.4	1.296	1.021	245.6
10.00	30.00	2073	4794.7	11.290	1.2334	.9218	.621	0.00071	2.155	354.4	1.204	1.262	301.8
20.00	15.00	1812	4558.0	11.290	1.2432	.8940	.565	0.00063	2.542	375.7	1.481	1.701	334.2
20.41	14.70	1805	4551.5	11.290	1.2435	.8930	.564	0.00063	2.554	376.3	1.530	1.700	335.0
40.00	7.50	1577	4351.5	11.290	1.2565	.8622	.509	0.00055	2.943	393.6	1.624	1.509	360.1
100.00	3.00	1302	4119.9	11.290	1.2742	.8178	.433	0.00042	3.434	412.6	1.0795	1.622	387.1
200.00	1.50	1118	3974.5	11.290	1.2890	.7621	.378	0.00038	3.809	424.5	1.774	1.651	405.3
400.00	.75	954	3846.3	11.290	1.3038	.7254	.325	0.00034	4.270	434.2	2.196	1.747	416.7
1000.00	.30	767	3708.0	11.290	1.3218	.7230	.264	0.00025	4.891	444.5	57.125	1.506	430.9
2000.00	.15	646	3622.0	11.290	1.3331	.7044	.220	0.00020	5.411	450.7	96.401	1.5842	439.5
4000.00	.08	542	3549.6	11.290	1.3527	.6890	.185	0.00017	5.980	455.9	159.954	1.6782	446.6
$R = 0.700$, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	300.00	3307	5138.3	12.574	1.2069	0.9217	.836	0.00094	0.000	836	1.206	0.000	0.0
1.05	285.71	3280	5112.9	12.574	1.2073	.9205	.832	0.00093	.285	566.7	1.172	.203	47.0
1.20	250.00	3205	5044.5	12.574	1.2082	.9172	.822	0.00092	.554	334.3	1.262	.390	90.3
1.40	214.29	3121	4967.4	12.574	1.2092	.9136	.810	0.00090	.757	297.9	1.062	.526	121.9
1.60	187.50	3049	4902.3	12.574	1.2101	.9103	.800	0.00089	.900	289.6	1.040	.618	145.3
1.78	168.68	2994	4851.6	12.574	1.2109	.9075	.792	0.00088	1.000	280.3	1.000	.681	157.9
2.00	150.00	2933	4796.6	12.574	1.2118	.9044	.783	0.00086	1.103	289.4	1.009	.743	177.4
4.00	75.00	2595	4494.6	12.574	1.2175	.8847	.731	0.00079	1.606	312.1	1.300	1.021	236.7
10.00	30.00	2197	4148.0	12.574	1.2257	.8521	.660	0.00070	2.155	345.0	2.220	1.266	293.5
20.00	15.00	1930	3922.2	12.574	1.2322	.8299	.602	0.00062	2.541	366.1	3.518	1.403	345.3
20.41	14.70	1922	3916.0	12.574	1.2325	.8290	.603	0.00062	2.552	366.6	3.567	1.400	326.1
40.00	7.50	1687	3724.3	12.574	1.2429	.8017	.548	0.00055	2.918	383.8	5.705	1.513	350.8
100.00	3.00	1402	3501.1	12.574	1.2618	.7018	.473	0.00045	3.422	403.9	11.013	1.628	377.4
200.00	1.50	1211	3358.2	12.574	1.2757	.7312	.416	0.00039	3.819	414.7	18.240	1.697	395.6
400.00	.75	1039	3232.5	12.574	1.2906	.7018	.361	0.00032	4.238	424.5	30.278	1.755	400.9
1000.00	.30	841	3099.5	12.574	1.3096	.6684	.294	0.00025	4.841	434.9	59.186	1.816	421.2
2000.00	.15	712	3014.7	12.574	1.3227	.6678	.248	0.00021	5.343	441.2	98.189	1.854	429.9
4000.00	.08	600	2943.0	12.574	1.3336	.6318	.207	0.00017	5.894	446.5	162.738	1.883	437.1
$R = 0.800$, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	300.00	3393	4586.9	13.740	1.2033	0.8561	.864	0.00090	0.000	864	1.203	0.000	0.0
1.05	285.71	3365	4563.0	13.740	1.2036	.8551	.860	0.00089	.285	510.4	2.170	.202	45.5
1.20	250.00	3290	4498.0	13.740	1.2044	.8522	.849	0.00088	.555	324.0	1.261	.389	87.6
1.40	214.29	3204	4426.0	13.740	1.2054	.8488	.837	0.00086	.758	288.8	1.052	.522	116.2
1.60	187.50	3132	4365.2	13.740	1.2062	.8460	.827	0.00085	.901	280.8	1.009	.617	138.9
1.78	168.91	3077	4318.3	13.740	1.2069	.8437	.819	0.00084	1.000	279.5	1.000	.680	152.9
2.00	150.00	3015	4266.0	13.740	1.2077	.8409	.810	0.00083	1.104	280.6	1.009	.743	167.1
4.00	75.00	2673	3981.2	13.740	1.2131	.8234	.750	0.00076	1.607	302.8	1.303	1.021	229.6
10.00	30.00	2270	3654.3	13.740	1.2216	.7974	.687	0.00067	2.157	335.0	2.229	1.266	284.9
20.00	15.00	1998	3440.4	13.740	1.2294	.7750	.632	0.00060	2.540	355.0	3.539	1.404	312.8
20.41	14.70	1990	3434.8	13.740	1.2297	.7743	.630	0.00060	2.551	356.2	3.590	1.408	316.6
40.00	7.50	1752	3252.9	13.740	1.2391	.7496	.572	0.00053	2.915	373.0	5.753	1.515	340.7
100.00	3.00	1462	3040.4	13.740	1.2542	.7136	.499	0.00045	3.416	391.9	11.146	1.631	366.8
200.00	1.50	1266	2953.8	13.740	1.2676	.6852	.441	0.00038	3.808	403.5	18.214	1.701	382.7
400.00	.75	1091	2785.9	13.740	1.2822	.6572	.385	0.00032	4.220	413.2	30.827	1.700	395.9
1000.00	.30	887	2655.2	13.740	1.3015	.6243	.316	0.00025	4.811	423.6	60.499	1.823	410.0
2000.00	.15	753	2573.1	13.740	1.3153	.6034	.268	0.00021	5.303	429.9	100.040	1.861	418.6
4000.00	.08	636	2503.6	13.740	1.3272	.5867	.246	0.00017	5.841	435.2	167.192	1.893	425.8
$R = 0.900$, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	300.00	3430	4142.9	14.789	1.2013	0.8019	.683	0.00086	0.000	683	1.201	0.000	0.0
1.05	285.71	3402	4120.6	14.789	1.2016	0.8010	.679	0.00085	.286	494.7	2.169	.202	44.1
1.20	250.00	3327	4060.2	14.789	1.2024	.783	.603	0.00084	.555	314.0	1.261	.389	84.9
1.40	214.29	3242	3992.2	14.789	1.2023	.755	.626	0.00082	.759	280.0	1.064	.522	114.5
1.60	187.50	3169	3934.7	14.789	1.2041	.7926	.646	0.00081	.901	274.2	1.009	.617	134.6
1.78	169.04	3114	3893.9	14.789	1.2047	.7903	.624	0.00080	1.000	271.0	1.000	.679	146.1
2.00	150.00	3021	3841.4	14.789	1.2052	.7881	.628	0.00079	1.103	272.1	1.010	.743	162.0
4.00	75.00	2706	3573.5	14.789	1.2106	.7122	.725	0.00073	1.608	293.7	1.304	1.020	222.6
10.00	30.00	2303	3265.6	14.789	1.2168	.7486	.704	0.00063	2.157	324.0	2.234	1.267	216.3
20.00	15.00	2030	3064.0	14.789	1.2262	.7621	.653	0.00058	2.540	342.1	3.551	1.405	305.4
20.41	14.70	2023	3058.4	14.789	1.2260	.7272	.647	0.00058	2.5				

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio P _c /P	Static pressure, P, lb./sq.in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, Y	Specific heat, c _p , cal./lbm°K.	Viscosity, μ, micro poises	Thermal conductivity, k, cal./sec/inch°K.	Mach number M	Specific impulse in vacuum, I _{vac} , (lb.sec)/lb	Area ratio, ε	Thrust coefficient, C _t , (lb.sec)/lb	Specific impulse, I, (lb.sec)/lb	
<i>R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937</i>														
1.00	300.00	3437	3777.9	15.734	1.2004	0.7565	.890	0.00004	0.000	2.286	480.1	2.168	0.000	
1.02	285.71	3409	3756.8	15.734	1.2006	0.7558	.894	0.00004	0.000	2.286	480.1	2.024	42.8	
1.20	250.00	3332	3699.8	15.734	1.2014	0.7533	.881	0.00004	0.000	2.055	304.8	1.260	.389	
1.40	214.29	3242	3625.9	15.734	1.2023	0.7505	.869	0.00004	0.000	1.759	271.7	1.062	.525	
1.60	187.50	3176	3551.7	15.734	1.2031	0.7480	.858	0.00004	0.000	1.494	264.2	1.009	.617	
1.77	164.10	3121	3504.0	15.734	1.2038	0.7461	.850	0.00004	0.000	1.400	263.0	1.000	.679	
2.00	150.00	3055	3495.9	15.734	1.2045	0.7439	.841	0.00004	0.000	1.305	264.1	1.010	.742	
4.00	75.00	2715	3241.6	15.734	1.2095	0.7291	.787	0.00007	1.000	1.608	285.1	1.305	1.020	
10.00	30.00	2311	2951.0	15.734	1.2175	0.7070	.714	0.00002	2.157	315.6	2.236	1.267	268.4	
20.00	15.00	2039	2750.8	15.734	1.2249	0.6879	.558	0.00005	2.240	335.1	3.557	1.409	297.5	
20.41	14.70	2031	2755.0	15.734	1.2251	0.6873	.557	0.00006	2.251	335.7	3.607	1.409	298.3	
40.00	7.50	1792	2593.8	15.734	1.2339	0.6663	.603	0.0002	2.913	515.7	5.792	1.516	321.0	
100.00	3.00	1500	2403.2	15.734	1.2481	0.6354	.525	0.00042	3.410	369.7	11.253	1.633	345.8	
200.00	1.50	1303	2290.7	15.734	1.2600	0.6104	.467	0.00036	3.799	380.8	18.738	1.702	360.9	
400.00	.75	1126	2174.8	15.734	1.2749	0.5857	.410	0.00031	4.206	390.1	31.282	1.784	373.5	
1000.00	.35	719	2005.6	15.734	1.2942	0.5556	.340	0.00024	4.788	400.1	61.611	1.828	387.0	
2000.00	.15	703	1952.2	15.734	1.3003	0.5360	.291	0.00020	5.270	406.2	102.755	1.887	395.3	
4000.00	.08	603	1919.0	15.734	1.3209	0.5193	.246	0.0001	5.798	411.4	171.104	1.899	404.2	
<i>R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905</i>														
1.00	300.00	3247	2626.1	19.320	1.2021	0.6117	.918	0.00006	0.000	2.285	424.3	2.169	0.000	0.0
1.05	285.71	3270	2609.6	19.320	1.2024	0.6110	.913	0.00006	0.000	2.285	424.3	2.024	37.9	
1.20	250.00	3197	2556.2	19.320	1.2032	0.6090	.904	0.00006	0.000	2.285	424.3	1.261	.389	72.8
1.40	214.29	3115	2515.1	19.320	1.2041	0.6068	.889	0.00006	0.000	2.285	424.3	1.062	.525	98.2
1.60	187.50	3048	2474.8	19.320	1.2050	0.6047	.877	0.00006	0.000	2.285	424.3	1.009	.617	115.5
1.78	168.99	2992	2440.6	19.320	1.2056	0.6030	.869	0.00006	1.000	2.324	1.000	.679	127.0	
2.00	150.00	2933	2404.3	19.320	1.2065	0.6011	.858	0.00006	1.104	235.3	1.009	.743	138.9	
4.00	75.00	2600	2207.3	19.320	1.2217	0.5888	.600	0.0002	1.008	251.9	1.303	1.020	190.9	
10.00	30.00	2210	1981.0	19.320	1.2200	0.5705	.724	0.0002	2.157	278.7	2.232	1.266	236.9	
20.00	15.00	1947	1832.9	19.320	1.2217	0.5550	.665	0.0004	2.240	295.9	3.546	1.404	262.7	
20.41	14.70	1940	1826.8	19.320	1.2227	0.5545	.664	0.0004	2.251	296.3	3.597	1.408	263.4	
40.00	7.50	1709	1702.7	19.320	1.2366	0.5317	.607	0.0004	2.915	310.4	5.769	1.515	283.4	
100.00	3.00	1429	1525.2	19.320	1.2507	0.5151	.529	0.0002	3.414	326.2	11.194	1.634	305.3	
200.00	1.50	1240	1456.2	19.320	1.2650	0.4939	.472	0.0002	3.805	335.9	18.624	1.702	318.5	
400.00	.75	1070	1377.9	19.320	1.2765	0.4747	.416	0.0002	4.215	344.1	31.071	1.782	329.6	
1000.00	.35	873	1285.6	19.320	1.2950	0.4515	.347	0.0002	4.800	352.8	61.164	1.825	341.4	
2000.00	.15	743	1229.1	19.320	1.3097	0.4351	.299	0.0001	5.284	358.2	101.998	1.864	348.6	
4000.00	.08	630	1180.2	19.320	1.3212	0.4251	.255	0.0001	5.814	362.6	169.845	1.896	354.7	
<i>R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873</i>														
1.00	300.00	5193	2016.0	21.723	1.2098	0.5359	.710	0.00005	0.000	2.285	388.2	2.172	0.000	0.0
1.05	285.71	5077	2002.4	21.723	1.2071	0.5353	.706	0.00005	0.000	2.285	388.2	2.023	3.66	
1.20	250.00	5007	1965.1	21.723	1.2090	0.5314	.694	0.00005	0.000	2.285	388.2	1.262	.390	66.6
1.40	214.29	4926	1920.2	21.723	1.2072	0.5291	.680	0.00005	0.000	2.285	388.2	1.094	.526	89.9
1.60	187.50	4861	1887.7	21.723	1.2100	0.5271	.666	0.00005	0.000	2.285	388.2	1.010	.618	105.6
1.78	168.99	4809	1855.4	21.723	1.2108	0.5250	.656	0.00005	0.000	2.285	388.2	1.000	.681	116.4
2.00	150.00	4752	1810.6	21.723	1.2117	0.5230	.648	0.00005	1.003	213.3	1.009	.743	127.0	
4.00	75.00	4235	1668.3	21.723	1.2217	0.5125	.587	0.0004	1.806	230.0	1.300	1.021	174.4	
10.00	30.00	2062	1478.1	21.723	1.2265	0.4958	.508	0.0004	2.156	254.3	2.220	1.266	216.3	
20.00	15.00	1811	1395.9	21.723	1.2344	0.4817	.486	0.0003	2.241	269.8	3.519	1.403	239.7	
20.41	14.70	1804	1384.1	21.723	1.2347	0.4813	.486	0.0003	2.253	270.2	3.569	1.406	240.4	
40.00	7.50	1595	1247.9	21.723	1.2437	0.4666	.486	0.0003	2.919	282.9	5.710	1.513	256.5	
100.00	3.00	1119	1128.5	21.723	1.2599	0.4456	.311	0.0002	3.423	297.1	11.039	1.628	278.2	
200.00	1.50	1049	1104.0	21.723	1.2706	0.4292	.455	0.0002	3.850	305.8	18.315	1.698	290.1	
400.00	.75	962	981.4	21.723	1.2836	0.4126	.404	0.0002	4.237	313.1	30.473	1.756	300.0	
1000.00	.35	798	907.1	21.723	1.3046	0.3948	.329	0.0001	4.833	320.9	59.799	1.818	310.6	
2000.00	.15	677	860.4	21.723	1.3151	0.3822	.289	0.0001	5.326	325.6	99.507	1.856	317.1	
4000.00	.08	572	820.8	21.723	1.3270	0.3712	.247	0.0001	5.865	329.6	165.365	1.887	322.5	
<i>R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810</i>														
1.00	300.00	2723	1581.4	24.669	1.2103	0.4495	.665	0.00004	0.000	2.285	341.1	2.179	0.000	0.0
1.05	285.71	2679	1570.5	24.669	1.2107	0.4468	.660	0.00004	0.000	2.285	341.1	2.023	30.4	
1.20	250.00	2656	1544.1	24.669	1.2109	0.4470	.648	0.00004	0.000	2.285	341.1	1.265	.391	58.5
1.40	214.29	2568	1507.5	24.669	1.2121	0.4449	.635	0.00004	0.000	2.285	341.1	1.004	.527	78.9
1.60	187.50	2501	1482.5	24.669	1.2122	0.4441	.621	0.00004	0.000	2.285	341.1	1.010	.620	92.7
1.78	168.99	2492	1465.6	24.669	1.2123	0.4415	.610	0.00004	1.000	218.3	1.000	.685	102.5	
2.00	150.00	2431	1436.9	24.669	1.2124	0.4399	.600	0.00004	1.079	187.0	1.008	.745	111.5	
4.00	75.00	2112	1112.6	24.669	1.2230	0.4293	.537	0.0003	1.802	201.3	1.293	1.022	152.9	
10.00	30.00	1773	954.6	24.669	1.2413	0.4144	.555	0.0003	2.155	222.1	2.193	1.265	189.3	
20.00	15.00	1546	877.0	24.669	1.2492	0.402	.594	0.0003	2.245	235.4	3.457	1.400	209.5	
20.41	14.70	1540	874.5	24.669	1.2493	0.4021	.594	0.0003	2.256	235.7	3.505	1.403	210.0	
40.00	7.50	1393	796.4	24.669	1.2500	0.3988	.536	0.0003	2.929	246.5	5.575	1.507	225.6	
1000.00	3.00	1107	706.2	24.669	1.2705	0.3729</								

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_c , lb/inch ² abs.	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g°C)	Viscos- ity, μ , micro poises	Thermal conductivity, K , cal/(sec°C) ^{1/2}	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/sec/lb	Area ratio, ϵ	Thrust coefficient, C_t , lb-sec/lb	Specific impulse, I , lb-sec/lb
$R = 4.000$, PERCENT FUEL = 3.054, O/F = 31.788													
1.00	300.00	2372	1054.4	26.307	1.2311	0.4025	804	0.00040	0.000	2.187	0.000	0.0	0.0
1.05	285.71	2351	1045.7	26.307	1.2315	0.4018	799	0.00040	0.282	308.3	1.269	0.204	27.5
1.20	250.00	2292	1022.3	26.307	1.2328	0.4000	786	0.00039	0.549	195.4	1.269	0.392	52.9
1.40	214.29	2226	996.0	26.307	1.2345	0.3979	772	0.00038	0.750	173.9	1.066	0.529	71.3
1.60	187.50	2171	973.8	26.307	1.2357	0.3960	759	0.00037	0.892	168.9	1.011	0.621	85.7
1.79	167.18	2123	955.2	26.307	1.2369	0.3945	748	0.00037	1.000	168.0	1.000	0.689	92.9
2.00	150.00	2080	938.0	26.307	1.2380	0.3920	738	0.00036	1.094	168.6	1.006	0.747	100.6
4.00	75.00	1817	856.1	26.307	1.2455	0.3851	675	0.00032	1.598	181.2	1.426	1.023	137.8
10.00	30.00	1512	721.1	26.307	1.2570	0.3694	593	0.00028	2.155	199.5	2.165	1.263	170.3
20.00	15.00	1309	647.4	26.307	1.2669	0.3585	535	0.00028	2.549	211.1	3.393	1.396	188.2
20.41	14.70	1304	645.3	26.307	1.2672	0.3582	533	0.00024	2.560	211.4	3.439	1.400	188.7
40.00	7.50	1129	583.6	26.307	1.2777	0.3476	480	0.00021	2.940	220.7	5.440	1.502	202.4
100.00	3.00	921	512.9	26.307	1.2932	0.3352	411	0.00018	3.469	231.0	10.346	1.610	217.1
200.00	1.50	785	464.3	26.307	1.3061	0.3223	362	0.00017	3.890	237.3	16.992	1.675	225.8
400.00	.75	666	430.4	26.307	1.3193	0.3121	316	0.00013	4.338	242.4	27.857	1.729	233.0
1000.00	.30	531	389.1	26.307	1.3369	0.2998	261	0.00010	4.983	247.8	53.783	1.875	240.6
2000.00	.15	445	363.6	26.307	1.3495	0.2917	224	0.00009	5.521	251.1	88.429	1.819	245.2
4000.00	.08	371	342.4	26.307	1.3589	0.2880	190	0.00007	6.117	259.8	145.294	1.847	248.9
$R = 5.000$, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	300.00	2069	855.0	27.313	1.2437	0.3713	742	0.00034	0.000	2.194	0.000	0.0	0.0
1.05	285.71	2050	847.7	27.313	1.2442	0.3707	737	0.00034	0.281	402.4	2.194	0.205	25.2
1.20	250.00	1996	828.0	27.313	1.2456	0.3690	724	0.00033	0.546	178.9	1.272	0.394	48.4
1.40	214.29	1936	800.0	27.313	1.2473	0.3670	710	0.00033	0.747	159.2	1.066	0.531	65.3
1.60	187.50	1886	787.4	27.313	1.2488	0.3652	697	0.00032	0.888	154.5	1.012	0.623	76.7
1.80	166.43	1841	771.2	27.313	1.2501	0.3636	686	0.00031	1.000	153.6	1.000	0.694	85.4
2.00	150.00	1803	757.5	27.313	1.2514	0.3622	677	0.00031	1.050	154.1	1.007	0.748	92.1
4.00	75.00	1566	672.6	27.313	1.2596	0.3530	614	0.00027	1.594	165.3	1.279	1.023	126.0
10.00	30.00	1292	577.6	27.313	1.2721	0.3402	536	0.00023	2.154	181.7	2.139	1.262	155.4
20.00	15.00	1112	517.0	27.313	1.2825	0.3303	481	0.00020	2.553	194.0	3.334	1.393	171.5
20.41	14.70	1107	515.1	27.313	1.2829	0.3300	479	0.00020	2.564	194.3	3.380	1.397	171.9
40.00	7.50	952	465.1	27.313	1.2939	0.3203	424	0.00018	2.950	205.5	5.317	1.496	184.2
100.00	3.00	770	407.9	27.313	1.3106	0.3070	364	0.00014	3.491	209.6	10.036	1.603	197.2
200.00	1.50	651	372.1	27.313	1.3239	0.2974	319	0.00012	3.943	215.0	16.365	1.665	205.0
400.00	.75	546	342.9	27.313	1.3375	0.2883	277	0.00011	4.385	219.5	26.695	1.717	211.3
1000.00	.30	433	309.3	27.313	1.3545	0.2760	227	0.00008	5.056	224.2	51.130	1.770	217.9
2000.00	.15	361	289.4	27.313	1.3659	0.2727	193	0.00007	5.622	227.0	83.618	1.802	221.8
4000.00	.08	299	272.8	27.313	1.3702	0.2693	163	0.00006	6.246	229.3	136.832	1.829	225.1

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

(Equivalence ratio, R; oxidant-fuel ratio, O/F.)

(h) Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/in ² abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g·°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec·°K)	Mach number, M	Specific impulse in vacuum, I _v , sec	Area ratio, ε	Thrust coefficient, C _f , lb-sec/lb	Specific impulse, I, lb-sec/lb	
R = 0.150, PERCENT FUEL = 45.65, C/F = 1.190														
1.00	600.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000	.271	530.0	2.250	0.000 47.4	
1.05	571.43	1148	5287.7	4.416	1.3406	1.7710	311	0.00073	.000	.527	334.2	1.297	4.03 90.8	
1.20	500.00	1129	5218.6	4.416	1.3456	1.7597	303	0.00070	.000	.722	296.1	1.081	5.43 122.2	
1.40	428.57	1085	5141.8	4.416	1.3469	1.7472	293	0.00068	.000	.860	286.6	1.018	6.36 143.2	
1.60	375.00	1049	5077.7	4.416	1.3497	1.7369	285	0.00066	.000	.980	276.0	1.000	7.25 163.4	
1.87	321.66	1008	5006.8	4.416	1.3528	1.7257	276	0.00063	1.000	1.000	284.1	1.003	7.61 171.5	
2.00	300.00	989	4975.4	4.416	1.3540	1.7210	272	0.00062	1.059	1.059	284.4	1.003	7.61 171.5	
4.00	150.00	824	4693.4	4.416	1.3651	1.6625	234	0.00052	1.566	301.7	1.233	1.031	232.3	
10.00	60.00	643	4392.5	4.416	1.3748	1.6505	188	0.00042	2.152	327.5	1.974	1.257	283.1	
20.00	30.00	532	4209.8	4.416	1.3799	1.6344	159	0.00035	2.586	343.5	2.982	1.376	309.9	
40.00	15.00	439	4058.9	4.416	1.3824	1.6268	133	0.00029	3.031	356.4	4.620	1.467	350.4	
40.83	14.70	437	4054.8	4.416	1.3825	1.6266	134	0.00029	3.044	356.8	4.682	1.469	350.9	
100.00	6.00	340	3899.0	4.416	1.3882	1.6093	104	0.00023	3.648	369.8	8.432	1.558	350.8	
200.00	3.00	280	3806.2	4.416	1.3926	1.5961	85	0.00018	4.149	377.7	13.431	1.610	362.6	
400.00	1.50	230	3723.2	4.416	1.4068	1.5562	70	0.00015	4.675	384.1	21.488	1.652	372.0	
1000.00	.60	175	3640.1	4.416	1.4349	1.4847	55	0.00011	5.438	390.6	39.928	1.699	381.6	
2000.00	.30	142	3590.9	4.416	1.4550	1.4389	45	0.00009	6.056	394.3	63.572	1.719	387.2	
4000.00	.15	114	3551.2	4.416	1.4705	1.4065	36	0.00007	6.845	397.3	100.938	1.739	391.6	
R = 0.200, PERCENT FUEL = 38.65, C/F = 1.587														
1.00	600.00	1514	2969.7	5.216	1.3079	1.6183	402	0.00084	0.000	.274	592.4	2.233	0.000 49.3	
1.05	571.43	1497	2941.7	5.216	1.3090	1.6140	399	0.00083	.000	.533	348.6	1.289	4.00 94.6	
1.20	500.00	1450	2866.8	5.216	1.3120	1.6022	389	0.00081	.000	.733	309.3	1.077	5.39 127.4	
1.40	428.57	1398	2785.1	5.216	1.3155	1.5887	378	0.00078	.730	309.3	1.016	6.32 149.4		
1.60	375.00	1356	2713.2	5.216	1.3185	1.5772	369	0.00076	.869	299.6	1.000	7.16 169.2		
1.85	324.94	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	297.3	1.000	7.16 169.2		
2.00	300.00	1282	2601.1	5.216	1.3236	1.5584	353	0.00072	1.068	297.8	1.004	7.57 179.1		
4.00	150.00	1079	2290.0	5.216	1.3391	1.5046	307	0.00061	1.572	316.7	1.244	1.029	243.2	
10.00	60.00	852	1954.3	5.216	1.3558	1.4216	251	0.00048	4.148	344.7	2.009	1.257	297.2	
20.00	30.00	709	1748.8	5.216	1.3656	1.4232	213	0.00040	2.573	362.0	3.049	1.379	325.9	
40.00	15.00	588	1578.0	5.216	1.3715	1.4066	179	0.00034	3.010	376.0	4.739	1.472	348.0	
40.83	14.70	585	1573.4	5.216	1.3716	1.4062	178	0.00034	3.023	376.4	4.802	1.474	348.6	
100.00	6.00	458	1396.3	5.216	1.3771	1.3913	144	0.00026	3.619	390.2	8.679	1.565	370.0	
200.00	3.00	379	1288.2	5.216	1.3811	1.3807	117	0.00022	4.111	399.1	15.470	1.614	384.7	
400.00	1.50	312	1195.2	5.216	1.3861	1.3677	96	0.00018	4.638	406.1	22.296	1.662	394.9	
1000.00	.60	242	1099.0	5.216	1.3973	1.3400	74	0.00013	5.394	413.4	41.979	1.706	403.5	
2000.00	.30	198	1041.1	5.216	1.4126	1.2977	61	0.00011	6.014	417.4	67.687	1.733	409.7	
4000.00	.15	161	993.9	5.216	1.4350	1.2568	50	0.00009	6.704	421.1	108.754	1.754	414.6	
R = 0.250, PERCENT FUEL = 33.51, C/F = 1.984														
1.00	600.00	1817	1249.3	6.016	1.2855	1.4955	481	0.00092	0.000	.219	502.4	2.219	0.000 50.3	
1.05	571.43	1797	1220.2	6.016	1.2844	1.4917	477	0.00091	.276	563.4	2.219	2.207	50.3	
1.20	500.00	1745	1142.1	6.016	1.2870	1.4813	467	0.00089	.538	356.2	1.283	3.398	96.6	
1.40	428.57	1686	1054.7	6.016	1.2900	1.4694	456	0.00086	.736	316.3	1.073	5.36	130.1	
1.60	375.00	1636	981.5	6.016	1.2946	1.4591	446	0.00083	.876	306.0	1.015	6.69	152.7	
1.83	327.79	1586	909.9	6.016	1.2974	1.4485	436	0.00081	1.000	304.5	1.000	7.03	171.8	
2.00	300.00	1555	864.0	6.016	1.2973	1.4415	429	0.00080	1.076	305.1	1.005	7.54	183.1	
4.00	150.00	1322	535.2	6.016	1.3125	1.3873	378	0.00060	1.579	325.3	1.226	1.027	249.3	
10.00	60.00	1057	176.3	6.016	1.3329	1.3222	314	0.00054	2.147	355.3	2.048	1.558	305.6	
20.00	30.00	887	9954.2	6.016	1.3461	1.2848	269	0.00046	2.563	373.7	3.127	1.384	335.7	
40.00	15.00	740	9786.3	6.016	1.3569	1.2559	228	0.00038	2.987	388.6	4.883	1.478	359.0	
40.83	14.70	736	9763.3	6.016	1.3572	1.2551	227	0.00038	3.000	389.0	4.949	1.481	359.6	
100.00	6.00	580	9569.3	6.016	1.3663	1.2320	181	0.00030	3.581	404.2	8.985	1.575	382.3	
200.00	3.00	481	9448.1	6.016	1.3717	1.2191	151	0.00025	4.064	413.4	14.395	1.630	395.9	
400.00	1.50	399	9347.6	6.016	1.3735	1.2100	124	0.00020	4.582	420.9	23.207	1.675	406.8	
1000.00	.60	310	9240.9	6.016	1.3821	1.1948	95	0.00015	5.327	428.7	43.891	1.722	418.0	
2000.00	.30	256	9176.3	6.016	1.3885	1.1802	78	0.00012	5.945	433.4	71.275	1.749	424.7	
4000.00	.15	210	9123.1	6.016	1.4049	1.1482	64	0.00010	6.606	437.1	115.642	1.771	430.1	
R = 0.300, PERCENT FUEL = 29.57, C/F = 2.381														
1.00	600.00	2094	9932.7	6.815	1.2647	1.3934	551	0.00097	0.000	.278	568.6	2.208	0.000 50.8	
1.05	571.43	2073	9905.1	6.815	1.2624	1.3904	547	0.00096	.278	.542	359.8	1.278	3.396	97.5
1.20	500.00	1951	9823.5	6.815	1.2675	1.3817	537	0.00094	.542	319.8	1.071	5.33	131.4	
1.40	428.57	1911	9734.4	6.815	1.2701	1.3714	525	0.00091	.761	310.2	1.013	6.26	154.2	
1.60	375.00	1896	9659.5	6.815	1.2724	1.3622	515	0.00089	.881	310.2	1.003	7.01	172.7	
1.82	330.00	1845	9589.9	6.815	1.2746	1.3534	505	0.00087	1.000	308.2	1.000	7.51	185.1	
2.00	300.00	1807	9539.0	6.815	1.2764	1.3467	498	0.00085	1.082	309.0	1.006	7.51	185.1	
4.00	150.00	1551	9200.2	6.815	1.2898	1.2980	444	0.00074	1.585	330.4	1.266	1.025	252.5	
10.00	60.00	1256	8826.3	6.815	1.3097	1.2332	375	0.00060	2.148	361.6	2.084	1.260	310.3	
20.00	30.00	1062	8592.4	6.815	1.3220	1.1888	325	0.00050	2.555	381.0	3.205	1.387	341.5	
40.00	15.00	894	8399.1	6.815	1.3305	1.1729	278	0.00042	2.969	396.8	5.035	1.483	365.8	
40.83	14.70	889	8389.8	6.815	1.3309	1.1720	277	0.00042	2.991	397.2	5.104	1.488	366.4	
100.00	6.00	706	8182.2	6.815	1.3732	1.1173	223	0.00035	3.545	413.2	9.321	1.585	390.3	
200.00	3.00	599	8051.7	6.815	1.3605	1.1006	187	0.00027	4.014	429.0	14.986	1.643	404.6	
40														

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s lb/in. ² abs.	Temperature, T_s °K	Enthalpy, h_s cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p cal/(g·°K)	Viscosity, μ micro poises	Thermal conductivity, k_s cal/(sec·°K·cm)	Mach number M	Specific impulse in vacuum, vac. (lb sec./lb)	Area ratio, ϵ	Thrust coefficient, C_f (lb sec./lb)	Specific impulse, I_{sp} (lb sec./lb)	
$R = 0.350, \text{ PERCENT FUEL} = 26.47, \text{ O/F} = 2.778$														
1.00	600.00	2347	8892.8	7.610	1.2500	1.3056	611	0.00100	0.000	0.000	0.000	0.000	0.000	
1.05	571.43	2324	8863.0	7.610	1.2507	1.3029	607	0.00099	0.280	569.9	2.199	0.205	50.9	
1.20	500.00	2263	8783.0	7.610	1.2525	1.2955	597	0.00097	0.545	360.6	1.274	0.394	97.7	
1.40	428.57	2193	8693.3	7.610	1.2546	1.2868	585	0.00094	0.745	320.9	1.069	0.532	131.7	
1.60	375.00	2135	8617.9	7.610	1.2565	1.2793	575	0.00092	0.886	311.5	1.012	0.624	154.7	
1.81	331.93	2082	8550.7	7.610	1.2582	1.2724	566	0.00090	1.000	309.6	1.000	0.696	172.5	
2.00	300.00	2039	8496.3	7.610	1.2597	1.2665	558	0.00089	1.087	310.5	1.007	0.749	185.7	
4.00	150.00	1763	8152.6	7.610	1.2714	1.2233	504	0.00078	1.590	332.7	1.274	1.024	253.8	
10.00	60.00	1443	7770.0	7.610	1.2893	1.1638	424	0.00064	2.150	365.0	2.116	1.261	312.6	
20.00	30.00	1231	7528.4	7.610	1.3043	1.1192	379	0.00055	2.551	385.2	3.276	1.390	344.6	
40.00	15.00	1044	7322.8	7.610	1.3196	1.0783	328	0.00046	2.954	401.7	5.180	1.491	369.6	
40.83	14.70	1034	7317.2	7.610	1.3200	1.0772	326	0.00046	2.966	402.1	5.252	1.494	370.3	
100.00	6.00	832	7099.0	7.610	1.3371	1.0358	266	0.00036	3.513	419.0	9.659	1.594	395.1	
200.00	3.00	697	6960.9	7.610	1.3440	1.0115	224	0.00030	3.967	429.3	15.596	1.654	410.0	
400.00	1.50	582	6645.4	7.610	1.3558	0.9950	187	0.00025	4.457	437.8	25.296	1.703	422.1	
1000.00	.60	457	6721.6	7.610	1.3638	0.9790	147	0.00019	5.166	446.6	48.178	1.754	434.6	
2000.00	.30	379	6646.1	7.610	1.3688	0.9693	120	0.00016	5.756	451.9	76.663	1.784	442.1	
4000.00	.15	314	6583.5	7.610	1.3738	0.9597	97	0.00013	6.399	456.2	128.622	1.809	448.3	
$R = 0.400, \text{ PERCENT FUEL} = 23.95, \text{ O/F} = 3.175$														
1.00	600.00	2574	8050.5	8.396	1.2385	1.2292	663	0.00101	0.000	0.281	568.3	2.191	0.205	50.7
1.05	571.43	2550	8020.9	8.396	1.2390	1.2271	659	0.00100	0.547	360.0	1.271	0.393	97.5	
1.20	500.00	2485	7941.4	8.396	1.2405	1.2210	649	0.00098	0.748	320.4	1.067	0.530	131.4	
1.40	428.57	2412	7852.0	8.396	1.2423	1.2137	638	0.00096	0.890	311.1	1.012	0.622	154.3	
1.60	375.00	2350	7776.8	8.396	1.2439	1.2071	627	0.00094	1.000	309.4	1.000	0.692	171.6	
1.80	333.38	2296	7712.1	8.396	1.2454	1.2012	618	0.00093	1.091	310.3	1.007	0.748	185.4	
2.00	300.00	2249	7655.4	8.396	1.2468	1.1958	610	0.00091	1.159	333.1	1.281	1.023	253.7	
4.00	150.00	1956	7310.9	8.396	1.2566	1.1592	557	0.00081	1.595					
10.00	60.00	1615	6924.5	8.396	1.2724	1.1057	484	0.00068	2.152	366.2	2.143	1.262	313.0	
20.00	30.00	1398	6678.4	8.396	1.2803	1.0634	429	0.00058	2.548	346.9	3.338	1.393	345.5	
40.00	15.00	1186	6467.6	8.396	1.3013	1.0222	375	0.00049	2.944	404.0	5.310	1.697	371.1	
40.83	14.70	1181	6461.8	8.396	1.3018	1.0211	374	0.00049	2.955	404.5	5.384	1.699	371.8	
100.00	6.00	954	6236.1	8.396	1.3108	0.9745	308	0.00039	3.487	422.1	9.975	1.602	397.3	
200.00	3.00	804	6092.4	8.396	1.3337	0.9480	261	0.00032	3.927	432.9	16.185	1.665	412.8	
400.00	1.50	675	5971.1	8.396	1.3493	0.9241	220	0.00027	4.401	441.7	26.355	1.715	425.4	
1000.00	.60	532	5840.7	8.396	1.3551	0.9033	173	0.00021	5.088	451.0	50.405	1.768	438.5	
2000.00	.30	443	5760.9	8.396	1.3607	0.8928	143	0.00017	5.663	456.6	82.493	1.800	446.3	
4000.00	.15	369	5694.5	8.396	1.3661	0.8833	117	0.00013	6.288	461.2	135.208	1.826	452.8	
$R = 0.450, \text{ PERCENT FUEL} = 21.87, \text{ O/F} = 3.571$														
1.00	600.00	2773	7354.5	9.167	1.2292	1.1624	707	0.00101	0.000	0.281	568.3	2.191	0.205	50.7
1.05	571.43	2748	7325.3	9.167	1.2297	1.1604	704	0.00101	0.547	357.9	1.268	0.392	96.8	
1.20	500.00	2680	7246.7	9.167	1.2311	1.1550	694	0.00099	0.549	318.6	1.066	0.529	130.6	
1.40	428.57	2604	7158.4	9.167	1.2326	1.1487	682	0.00097	0.751	309.5	1.011	0.621	153.4	
1.60	375.00	2539	7084.0	9.167	1.2339	1.1433	672	0.00095	0.893	306.9	1.000	0.689	170.1	
1.79	334.56	2484	7021.9	9.167	1.2352	1.1386	663	0.00094	1.000	307.8	1.000	0.746	184.4	
2.00	300.00	2433	6963.8	9.167	1.2364	1.1338	655	0.00092	1.095	308.8	1.008	0.746	184.4	
4.00	150.00	2127	6621.6	9.167	1.2420	1.1016	602	0.00083	1.598	332.0	1.286	1.022	252.5	
10.00	60.00	1769	6239.4	9.167	1.2589	1.0541	529	0.00070	2.153	365.5	2.165	1.263	312.0	
20.00	30.00	1530	5987.8	9.167	1.2713	1.0157	474	0.00061	2.546	386.7	3.389	1.396	344.8	
40.00	15.00	1316	5776.3	9.167	1.2825	0.9761	418	0.00052	2.936	404.3	5.420	1.501	370.8	
40.83	14.70	1310	5768.5	9.167	1.2829	0.9750	417	0.00052	2.947	404.7	5.497	1.504	371.5	
100.00	6.00	1068	5653.2	9.167	1.3053	0.9267	348	0.00042	3.467	422.9	10.256	1.609	397.5	
200.00	3.00	905	5390.3	9.167	1.3195	0.8952	298	0.00035	3.895	434.1	16.723	1.674	413.4	
400.00	1.50	763	5265.1	9.167	1.3322	0.8693	252	0.00029	4.353	443.3	27.347	1.726	426.4	
1000.00	.60	605	5129.7	9.167	1.3452	0.8484	199	0.00022	5.021	453.0	52.536	1.781	440.0	
2000.00	.30	506	5046.4	9.167	1.3533	0.8303	165	0.00018	5.577	458.8	86.213	1.814	448.1	
4000.00	.15	422	4976.9	9.167	1.3599	0.8207	136	0.00015	6.187	463.6	141.612	1.841	454.8	
$R = 0.500, \text{ PERCENT FUEL} = 20.12, \text{ O/F} = 3.968$														
1.00	600.00	2944	5769.6	9.919	1.2218	1.1037	745	0.00101	0.000	0.281	559.4	2.181	0.204	49.9
1.05	571.43	2918	5741.0	9.919	1.2224	1.1020	741	0.00100	0.551	554.7	1.266	0.391	95.9	
1.20	500.00	2846	5663.8	9.919	1.2234	1.0971	731	0.00099	0.753	520.9	1.005	0.528	129.4	
1.40	428.57	2769	5577.1	9.919	1.2240	1.0914	720	0.00097	0.895	506.9	1.011	0.620	152.0	
1.60	375.00	2702	5503.9	9.919	1.2261	1.0865	710	0.00095	1.000	505.4	1.000	0.686	168.3	
1.79	335.48	2647	5444.3	9.919	1.2272	1.0823	701	0.00093	1.097	506.4	1.008	0.745	182.8	
2.00	300.00	2592	5385.6	9.919	1.2282	1.0781	693	0.00092	1.159	529.7	1.291	1.022	250.6	
4.00	150.00	2275	5048.0	9.919	1.2358	1.0500	640	0.00083	1.601	329.7	1.291	1.022	250.6	
10.00	60.00	1904	5665.2	9.919	1.2480	1.0081	568	0.00072	2.154	363.5	2.183	1.264	310.0	
20.00	30.00	1655	5418.4	9.919	1.2593	0.9730	513	0.00063	2.544	385.0	3.431	1.398	342.9	
40.00	15.00	1431	5204.5	9.919	1.2724	0.9359	457	0.00054	2.930	402.8	5.512	1.505	369.0	
40.83	14.70	1424	5198.6	9.919	1.2728	0.9348	455	0.00054	2.941	403.3	5.591	1.508	369.7	
100.00	6.00	117												

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/inch ²	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/deg·K	Viscosity, μ, poises	Thermal conductivity, k, cal/sec·cm ² ·deg	Mach number, M	Specific impulse in vacuum, I _{vac} , lb-sec/lb	Area ratio, ε	Thrust coefficient, C _t	Specific impulse, I, lb-sec/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.752													
1.00	600.00	3208	5841.6	11.347	1.2112	1.0044	803	0.00028	0.000	0.000	0.000	0.000	0.000
1.05	571.43	3186	5614.3	11.347	1.2115	1.0031	600	0.00026	.284	546.0	2.175	.263	48.7
1.20	500.00	3107	5740.3	11.347	1.2122	.9994	790	0.00026	.553	546.4	1.263	.390	93.7
1.40	428.57	3024	5958.1	11.347	1.2130	.9990	778	0.00026	.756	598.4	1.065	.526	126.4
1.60	375.00	2954	5983.2	11.347	1.2136	.9910	768	0.00026	.898	590.0	1.040	.519	146.5
1.78	336.81	2898	5953.1	11.347	1.2139	.9877	760	0.00026	1.000	298.0	1.000	.562	163.6
2.00	300.00	2857	5975.0	11.347	1.2165	.9841	754	0.00026	1.011	299.7	1.009	.744	178.6
4.00	150.00	2508	5105.9	11.347	1.2227	.9516	700	0.00025	1.054	323.0	1.298	1.021	245.1
10.00	60.00	2112	4780.9	11.347	1.2328	.9274	627	0.00024	2.456	355.8	2.209	1.262	305.8
20.00	30.00	1891	4500.2	11.347	1.2424	.8962	574	0.00024	2.442	378.4	3.492	1.404	350.5
40.00	15.00	1613	4330.4	11.347	1.2532	.8660	519	0.00026	2.422	396.5	5.948	1.510	362.6
40.83	14.70	1607	4324.7	11.347	1.2536	.8558	516	0.00026	2.433	397.0	5.730	1.513	362.3
100.00	6.00	1334	4049.6	11.347	1.2707	.8224	442	0.00026	3.451	416.0	10.859	1.624	307.9
200.00	3.00	1148	3944.0	11.347	1.2821	.7859	387	0.00024	3.453	427.9	17.925	1.696	406.3
400.00	1.50	981	3815.0	11.347	1.2999	.7540	334	0.00023	4.260	437.7	27.054	1.749	417.9
1000.00	.60	790	3673.4	11.347	1.3181	.7288	270	0.00023	4.676	446.4	57.768	1.803	436.4
2000.00	.30	667	3589.1	11.347	1.3299	.7060	227	0.00021	5.391	354.6	92.210	1.848	442.1
4000.00	.15	560	3510.6	11.347	1.3397	.6905	167	0.00017	5.955	439.6	157.552	1.876	450.3
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	600.00	3381	5138.3	12.064	1.2044	0.9246	846	0.00035	0.000	0.000	0.000	0.000	0.000
1.05	571.43	3353	5112.5	12.064	1.2047	0.9234	842	0.00034	.285	530.7	2.171	.203	47.4
1.20	500.00	3270	5043.0	12.064	1.2056	0.9201	852	0.00033	.554	536.0	1.262	.389	91.0
1.40	428.57	3196	4996.8	12.064	1.2066	0.9164	820	0.00031	.759	520.2	1.082	.525	122.4
1.60	375.00	3120	4898.7	12.064	1.2070	0.9132	810	0.00030	.900	241.9	1.009	.618	144.4
1.78	337.67	3064	4877.8	12.064	1.2062	0.9106	804	0.00030	1.000	290.6	1.000	.680	159.0
2.00	300.00	3004	4791.5	12.064	1.2090	0.9076	793	0.00030	1.033	291.7	1.009	.743	175.7
4.00	150.00	2680	4483.9	12.064	1.2146	0.8992	744	0.00030	1.067	314.7	1.207	1.021	250.0
10.00	60.00	2227	4131.1	12.064	1.2233	.8599	674	0.00024	2.451	340.1	2.220	1.265	270.0
20.00	30.00	1992	3900.7	12.064	1.2314	.8299	617	0.00024	2.421	359.4	3.232	1.404	320.2
40.00	15.00	1736	3690.4	12.064	1.2413	.8071	561	0.00026	2.416	367.5	5.757	1.514	324.0
40.83	14.70	1732	3692.6	12.064	1.2416	.8053	556	0.00026	2.427	366.0	5.021	1.517	324.6
100.00	6.00	1448	3469.6	12.064	1.2586	.7679	486	0.00027	3.418	407.0	11.400	1.632	381.0
200.00	3.00	1259	3232.0	12.064	1.2704	.7572	424	0.00026	3.612	419.0	18.418	1.700	397.4
400.00	1.50	1078	3196.4	12.064	1.2851	.7073	370	0.00024	4.226	429.0	30.655	1.758	411.1
1000.00	.60	875	3056.3	12.064	1.3043	.6726	307	0.00027	4.822	439.7	60.059	1.820	429.6
2000.00	.30	742	2968.5	12.064	1.3177	.6586	286	0.00024	5.317	446.2	99.783	1.855	430.5
4000.00	.15	627	2894.2	12.064	1.3271	.6357	217	0.00018	5.860	452.6	162.547	1.890	441.9
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.939													
1.00	600.00	3481	4586.9	13.859	1.2004	0.8591	873	0.00021	0.000	0.000	0.000	0.000	0.000
1.05	571.43	3453	4522.0	13.859	1.2006	0.8580	874	0.00020	.286	514.8	2.168	.204	45.9
1.20	500.00	3270	4523.0	13.859	1.2026	0.8552	861	0.00019	.555	526.0	1.260	.389	88.3
1.40	428.57	3290	4423.6	13.859	1.2026	0.8519	849	0.00018	.759	291.4	1.082	.522	119.2
1.60	375.00	3217	4361.3	13.859	1.2032	0.8490	839	0.00018	.904	285.5	1.009	.617	140.1
1.78	338.19	3161	4314.0	13.859	1.2039	0.8466	831	0.00018	1.000	284.1	1.000	.671	154.1
2.00	300.00	3098	4280.3	13.859	1.2046	0.8444	826	0.00018	1.025	283.2	1.010	.742	165.6
4.00	150.00	2750	3969.9	13.859	1.2097	0.8273	770	0.00018	1.088	305.7	1.304	1.020	231.7
10.00	60.00	2341	3636.1	13.859	1.2177	.8024	700	0.00019	2.157	358.4	2.236	1.267	287.6
20.00	30.00	2065	3417.4	13.859	1.2224	.7603	640	0.00022	2.494	359.4	3.556	1.405	319.0
40.00	15.00	1814	3229.8	13.859	1.2324	.7557	590	0.00022	2.413	371.1	5.791	1.516	344.3
40.83	14.70	1807	3219.5	13.859	1.2349	.7549	560	0.00022	2.424	371.6	5.670	1.519	344.9
100.00	.60	518	3004.4	13.859	1.2505	.7203	514	0.00016	3.410	396.4	11.247	1.633	370.8
200.00	.30	3119	2802.0	13.859	1.2620	.6916	457	0.00016	3.795	405.3	16.742	1.704	387.0
400.00	1.50	1137	2745.0	13.859	1.2706	.6630	401	0.00014	4.207	416.2	31.621	1.764	400.5
1000.00	.60	929	2608.0	13.859	1.2921	.6294	350	0.00017	4.789	426.9	51.524	1.827	415.0
2000.00	.30	791	2522.7	13.859	1.3091	.6073	281	0.00017	5.274	435.5	104.579	1.866	423.0
4000.00	.15	670	2450.2	13.859	1.3126	.5593	237	0.00018	5.801	440.9	170.764	1.899	431.2
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.243													
1.00	600.00	3528	4142.9	14.930	1.1982	0.8047	896	0.00017	0.000	0.000	0.000	0.000	0.000
1.05	571.43	3498	4120.1	14.930	1.1983	0.8036	892	0.00017	.286	494.2	2.167	.204	44.9
1.20	500.00	3421	4056.7	14.930	1.1984	0.8034	881	0.00019	.555	517.0	1.260	.389	62.0
1.40	428.57	3359	3957.4	14.930	1.2001	0.7963	869	0.00019	.759	284.0	1.082	.522	119.6
1.60	375.00	3261	3930.8	14.930	1.2009	0.7956	857	0.00019	.904	284.5	1.009	.617	135.7
1.78	335.45	3205	3858.0	14.930	1.2019	0.7936	851	0.00019	1.000	283.0	1.000	.678	144.5
2.00	300.00	3141	3825.7	14.930	1.2046	0.7913	844	0.00019	1.036	284.6	1.010	.742	165.5
4.00	150.00	2792	3552.3	14.930	1.2470	.7760	787	0.00019	1.099	296.7	1.300	1.020	224.8
10.00	60.00	2381	3247.3	14.930	1.2446	.7253	719	0.00020	2.157	326.0	2.241	1.267	274.2
20.00	30.00	2103	3040.7	14.930	1.2518	.7252	664	0.00020	2.439	349.0	3.569	1.406	309.7
40.00	15.00	1851	2858.3	14.930	1.2604	.7107	606	0.00019	2.911	366.4	5.660	1.517	334.5
40.83	14.70	1844	2855.2	14.930	1.2606	.7102	598	0.00019	2.942	366.8	5.706	1.510	335.0
100.00	.60	1553	2651.4	14.930	1.2691	.6794	524	0.00019	3.406	395.6	11.328	1.632	360.3
200.00	.30	1354	2517.0	14.930	1.2708	.6593	479	0.00019	3.792	396.9	18.572	1.761	376.1
400.00	.15	1170	2401.4	14.930</									

TABLE II. - Concluded. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P ₀	Static pressure, P, lb/inch ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	ISENTROPIC exponent, Y	Specific heat, c _p , cal/10 ⁶ °K/cm	Viscosity, μ, micro poises	Thermal conductivity, k, cal/sec°K/cm	Mach number, M	Specific impulse in vacuum, I _{vac} , sec/10 ⁻³	Area ratio, E	Thrust coefficient, C _F	Specific impulse, I, lbsec/lb
R = 1.000, PERCENT FUEL = 11.19%, O/F = 7.937													
1.00	600.00	3534	3777.49	15.886	1.1972	0.7592	910	0.00083	0.000	484.5	2.166	0.000	0.0
1.05	571.43	3505	3756.4	15.886	1.1975	0.7584	906	0.00083	.286	484.5	2.162	.202	43.2
1.20	500.00	3429	3696.5	15.886	1.1984	0.7560	893	0.00082	.556	307.6	1.260	.389	83.1
1.40	428.57	3342	3635.2	15.886	1.1991	0.7533	882	0.00080	.760	275.3	1.061	.525	112.2
1.60	375.00	3269	3576.0	15.886	1.1999	0.7503	874	0.00079	.903	266.8	1.009	.617	131.9
1.77	338.59	3214	3536.6	15.886	1.2005	0.7489	864	0.00078	1.000	265.6	1.000	.677	144.9
2.00	300.00	3149	3488.4	15.886	1.2012	0.7466	854	0.00077	1.105	266.7	1.010	.742	158.7
4.00	150.00	2801	3230.7	15.886	1.2029	0.7327	801	0.00071	1.609	288.1	1.307	1.020	218.2
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	600.00	2390	2955.7	15.886	1.2153	0.7115	730	0.00065	2.157	319.0	2.244	1.267	271.0
1.05	590.00	2312	2738.7	15.886	1.2104	0.6921	674	0.00067	4.539	336.9	3.575	1.406	300.7
1.20	530.00	1861	2566.6	15.886	1.2187	0.6720	616	0.00061	2.911	355.8	5.835	1.518	344.6
1.40	440.83	1470	1853	15.886	1.2220	0.6714	516	0.00051	2.922	356.3	5.919	1.521	325.3
1.60	360.00	600	1565	15.886	1.2241	0.6414	542	0.00043	3.404	374.2	11.363	1.636	349.9
2.00	300.00	300	1362	15.886	1.2253	0.6169	484	0.00037	3.789	385.6	18.966	1.708	365.3
4.00	150.00	1160	1234.2	15.886	1.2270	0.5921	428	0.00032	4.192	395.2	31.744	1.768	376.2
1000.00	.80	967	2011.2	15.886	1.2670	0.5609	356	0.00026	4.764	405.5	62.740	1.833	392.0
2000.00	.30	826	1933.9	15.886	1.3013	0.5403	308	0.00021	5.238	411.8	104.909	1.873	400.6
4000.00	.15	701	1867.0	15.886	1.3145	0.5220	260	0.00018	5.755	417.0	175.109	1.906	407.7
R = 2.000, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	600.00	3374	2626.1	19.463	1.1996	0.6136	930	0.00069	0.000	0.000	0.000	0.000	0.0
1.05	571.43	3346	2609.3	19.463	1.1999	0.6129	922	0.00069	.286	427.7	2.168	.402	38.2
1.20	500.00	3273	2564.2	19.463	1.2007	0.6109	914	0.00067	.555	471.5	1.260	.389	73.4
1.40	428.57	3189	2513.4	19.463	1.2016	0.6086	901	0.00066	.759	424.1	1.061	.525	99.0
1.60	375.00	3118	2470.4	19.463	1.2023	0.6067	889	0.00065	.904	435.4	1.009	.617	116.4
1.77	338.29	3065	2437.8	19.463	1.2030	0.6051	881	0.00065	1.000	434.4	1.000	.678	128.0
2.00	300.00	3003	2406.0	19.463	1.2037	0.6032	871	0.00064	1.105	425.5	1.010	.742	140.1
4.00	150.00	2668	2200.2	19.463	1.2068	0.5912	813	0.00058	1.609	254.1	1.305	1.020	192.5
10.00	60.00	2272	1969.5	19.463	1.2166	0.5735	737	0.00052	2.157	281.2	2.238	1.267	239.0
20.00	30.00	2002	1818.1	19.463	1.2238	0.5283	679	0.00047	2.539	298.7	3.561	1.402	262.1
40.00	15.00	1763	1655.2	19.463	1.2225	0.5113	540	0.00042	2.915	313.5	5.802	1.517	286.1
40.83	14.70	1756	1651.5	19.463	1.2321	0.5040	519	0.00041	2.924	313.7	5.867	1.519	286.7
1000.00	.80	1477	1583.9	19.463	1.2460	0.5172	543	0.00035	3.409	299.6	11.282	1.634	308.3
2000.00	.30	1285	1436.3	19.463	1.2579	0.4979	486	0.00030	3.797	339.0	18.804	1.702	321.8
4000.00	.15	1112	1351.6	19.463	1.2711	0.4787	430	0.00026	4.203	347.6	31.433	1.762	333.0
10000.00	.05	909	1297.3	19.463	1.2895	0.4486	360	0.00021	4.781	356.8	62.045	1.829	349.1
20000.00	.030	776	1197.7	19.463	1.3034	0.4355	312	0.00018	5.259	364.5	103.674	1.868	352.5
40000.00	.015	657	1147.0	19.463	1.3150	0.4252	266	0.00015	5.780	366.9	172.958	1.901	358.7
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	600.00	3158	2016.0	21.832	1.2049	0.5352	919	0.00060	0.000	0.000	0.000	0.000	0.0
1.05	571.43	3132	2004.1	21.832	1.2049	0.5346	915	0.00059	.285	390.6	2.171	.204	34.9
1.20	500.00	3051	1964.0	21.832	1.2049	0.5288	903	0.00058	.554	247.9	1.262	.389	67.0
1.40	428.57	2984	1922.0	21.832	1.2071	0.5206	889	0.00057	.756	221.0	1.062	.528	90.4
1.60	375.00	2914	1887.2	21.832	1.2050	0.5165	877	0.00056	.900	214.8	1.010	.610	106.3
1.77	337.61	2861	1858.2	21.832	1.2049	0.5170	866	0.00056	1.000	213.9	1.000	.680	117.0
2.00	300.00	2804	1828.2	21.832	1.2050	0.5202	856	0.00055	1.103	214.7	1.009	.743	127.9
4.00	150.00	2483	1661.5	21.832	1.2151	0.5143	797	0.00050	1.607	213.6	1.302	1.021	175.6
10.00	60.00	2108	1473.2	21.832	1.2258	0.4717	718	0.00044	2.157	256.1	2.222	1.266	217.9
20.00	30.00	1892	1347.6	21.832	1.2316	0.4340	588	0.00039	2.541	271.9	3.530	1.403	241.5
50.00	15.00	1622	1258.4	21.832	1.2407	0.4092	599	0.00035	2.918	285.1	5.734	1.514	260.5
50.83	14.70	1615	1237.5	21.832	1.2409	0.4085	597	0.00035	2.929	285.5	5.818	1.517	261.0
1000.00	.80	1353	1112.6	21.832	1.2549	0.4461	521	0.00026	3.420	299.8	11.102	1.629	280.4
2000.00	.30	1172	1033.0	21.832	1.2669	0.4321	462	0.00023	3.814	308.5	18.444	1.700	292.5
4000.00	.15	1010	969.5	21.832	1.2800	0.4161	411	0.00022	4.228	319.7	30.751	1.758	304.5
10000.00	.05	822	805.1	21.832	1.2977	0.3965	344	0.00018	4.819	323.7	60.449	1.821	313.3
20000.00	.030	700	840.2	21.832	1.3100	0.3955	296	0.00017	5.205	326.5	100.076	1.859	314.9
40000.00	.015	592	797.5	21.832	1.3154	0.3725	259	0.00014	5.841	332.6	167.547	1.894	325.4
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	600.00	2747	1381.4	24.718	1.2174	0.4502	860	0.00048	0.000	0.000	0.000	0.000	0.0
1.05	571.43	2723	1370.7	24.718	1.2178	0.4495	862	0.00048	.284	342.5	2.179	.203	30.6
1.20	500.00	2659	1341.8	24.718	1.2189	0.4477	852	0.00047	.551	217.1	1.265	.391	56.7
1.40	428.57	2586	1302.3	24.718	1.2201	0.4456	832	0.00046	.754	193.4	1.054	.527	79.2
1.60	375.00	2524	1281.9	24.718	1.2212	0.4435	829	0.00045	.956	187.9	1.040	.619	95.1
1.77	336.36	2475	1255.6	24.718	1.2222	0.4413	819	0.00044	1.000	187.0	1.000	.680	106.8
2.00	300.00	2424	1237.4	24.718	1.2234	0.4406	805	0.00044	1.099	187.1	1.007	.742	111.9
4.00	150.00	2133	1110.7	24.718	1.2289	0.4301	741	0.00037	1.604	204.1	1.274	1.022	155.5
10.00	60.00	1762	960.4	24.718	1.2401	0.4152	657	0.00034	2.156	220.0	2.159	1.263	190.0
20.00	30.00	1564	873.0	24.718	1.2409	0.4054	599	0.00030	2.545	236.0	3.481	1.400	210.3
40.00	15.00	1337	791.7	24.718	1.2411	0.3907	540	0.00027	2.928	247.3	5.506	1.500	226.5
40.83	14.70	1313	787.5	24.718	1.2417	0.3903	539	0.00026	2.940	247.8	5.607	1.510	226.9
1000.00	.80	604	538.4	24.718	1.2512	0.3734	467	0.00022	3.444				

TABLE II. - Concluded. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN
 [Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s , lb/inch ²	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, \bar{M}	ISENTROPIC exponent, γ	Specific heat, c_p , cal/(g°C)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(inch°K)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb/sec/lb	Area ratio, e	Thrust coefficient, C_F	Specific impulse, I , lb/sec/lb
$R = 4.000$, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	600.00	2381	1054.4	26.323	1.2307	0.4027	806	0.00040	0.000	0.000	0.000	0.000	0.0
1.05	571.43	2359	1045.7	26.323	1.2312	0.4021	801	0.00040	.282	308.7	2.187	.204	27.6
1.20	500.00	2300	1022.2	26.323	1.2325	0.4003	788	0.00039	.549	195.7	1.269	.392	52.9
1.40	428.57	2234	995.8	26.323	1.2340	0.3981	774	0.00038	.750	174.2	1.066	.529	71.4
1.60	375.00	2176	973.6	26.323	1.2353	0.3963	761	0.00037	.892	169.2	1.011	.621	83.9
1.79	334.41	2131	954.9	26.323	1.2365	0.3947	750	0.00037	1.000	168.3	1.000	.689	93.0
2.00	300.00	2087	937.6	26.323	1.2376	0.3932	740	0.00036	1.094	168.8	1.008	.747	100.8
4.00	150.00	1824	835.4	26.323	1.2452	0.3833	676	0.00032	1.598	181.4	1.286	1.023	138.0
10.00	60.00	1518	720.1	26.323	1.2566	0.3697	595	0.00028	2.155	199.8	2.166	1.263	170.6
20.00	30.00	1315	646.1	26.323	1.2665	0.3588	537	0.00024	2.549	211.4	3.394	1.396	188.5
40.00	15.00	1134	582.1	26.323	1.2771	0.3479	481	0.00021	2.939	221.1	5.444	1.502	202.7
40.83	14.70	1129	580.3	26.323	1.2775	0.3476	480	0.00021	2.951	221.4	5.521	1.505	203.1
100.00	6.00	926	511.0	26.323	1.2927	0.3334	412	0.00018	3.469	231.4	10.356	1.611	217.4
200.00	3.00	789	466.2	26.323	1.3055	0.3226	363	0.00015	3.889	237.7	16.972	1.676	226.2
400.00	1.50	669	428.2	26.323	1.3187	0.3124	317	0.00013	4.336	242.8	27.895	1.729	233.4
1000.00	.60	534	386.7	26.323	1.3363	0.3000	262	0.00010	4.980	248.3	53.871	1.785	241.0
2000.00	.30	447	361.1	26.323	1.3489	0.2918	225	0.00009	5.518	251.6	88.590	1.819	245.6
4000.00	.15	373	339.7	26.323	1.3586	0.2860	191	0.00007	6.112	254.3	145.580	1.847	249.4
$R = 5.000$, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	600.00	2072	855.0	27.317	1.2436	0.3714	742	0.00034	0.000	0.000	0.000	0.000	0.0
1.05	571.43	2052	847.0	27.317	1.2441	0.3708	737	0.00034	.281	282.6	2.194	.205	25.2
1.20	500.00	1999	828.0	27.317	1.2455	0.3691	725	0.00033	.546	179.0	1.272	.394	48.5
1.40	428.57	1939	805.0	27.317	1.2472	0.3671	710	0.00033	.747	159.2	1.068	.531	65.3
1.60	375.00	1888	787.3	27.317	1.2487	0.3653	698	0.00032	.888	154.6	1.012	.623	76.7
1.80	332.87	1844	771.2	27.317	1.2500	0.3637	687	0.00031	1.000	153.7	1.000	.694	85.4
2.00	300.00	1806	757.4	27.317	1.2512	0.3623	677	0.00031	1.090	154.2	1.007	.748	92.2
4.00	150.00	1568	672.0	27.317	1.2595	0.3531	614	0.00027	1.594	165.4	1.279	1.023	126.0
10.00	60.00	1294	577.3	27.317	1.2720	0.3402	536	0.00023	2.154	181.8	2.139	1.262	155.4
20.00	30.00	1113	516.7	27.317	1.2824	0.3303	481	0.00020	2.553	192.1	3.335	1.393	171.6
40.00	15.00	953	464.7	27.317	1.2937	0.3204	429	0.00018	2.950	200.7	5.318	1.497	184.3
40.83	14.70	949	463.3	27.317	1.2940	0.3201	428	0.00018	2.962	200.9	5.393	1.499	184.6
100.00	6.00	771	407.4	27.317	1.3104	0.3071	364	0.00014	3.490	209.7	10.039	1.603	197.4
200.00	3.00	652	371.6	27.317	1.3237	0.2975	319	0.00012	3.923	215.2	16.351	1.665	205.1
400.00	1.50	549	341.3	27.317	1.3373	0.2884	277	0.00011	4.385	219.6	26.706	1.717	211.4
1000.00	.60	434	308.7	27.317	1.3544	0.2780	228	0.00008	5.055	224.3	51.154	1.770	218.0
2000.00	.30	361	288.7	27.317	1.3638	0.2727	193	0.00007	5.621	227.1	83.660	1.803	222.0
4000.00	.15	300	272.1	27.317	1.3701	0.2693	163	0.00006	6.245	229.4	136.905	1.829	225.2

TABLE III. - THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS
FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temp-erature, T , °K	Temp-erature exponent, n_1	Area ratio, ϵ	Area- ratio exponent, n_2	Specific impulse, I , (lb/sec)/lb	Specific- impulse exponent, n_3	Specific heat, c_p , cal/(g·°K)	$(\partial \ln \mathcal{R}) / (\partial \ln P)_T$	$(\partial \ln \mathcal{R}) / (\partial \ln P)_P$
$R = 0.15$, PERCENT FUEL = 45.65, O/F = 1.190									
1.00	1183	0.0000							
1.05	1168	.0000	2.250	0.0000	47.4	0.0000	1.7753	0.00000	0.0000
1.20	1129	.0000	1.297	0.0000	90.8	0.0000	1.7597	0.00000	0.0000
1.40	1085	.0000	1.081	0.0000	122.2	0.0000	1.7472	0.00000	0.0000
1.60	1049	.0000	1.018	0.0000	143.2	0.0000	1.7369	0.00000	0.0000
1.87	1008	.0000	1.000	0.0000	163.4	0.0000	1.7257	0.00000	0.0000
2.00	989	.0000	1.003	0.0000	171.5	0.0000	1.7210	0.00000	0.0000
4.00	824	.0000	1.233	0.0000	232.3	0.0000	1.6826	0.00000	0.0000
4.08	819	.0000	1.244	0.0000	233.7	0.0000	1.6816	0.00000	0.0000
10.00	643	.0000	1.974	0.0000	283.1	0.0000	1.6507	0.00000	0.0000
20.00	532	.0000	2.983	0.0000	309.9	0.0000	1.6343	0.00000	0.0000
40.00	439	.0000	4.620	0.0000	330.4	0.0000	1.6268	0.00000	0.0000
100.00	340	.0000	8.432	0.0000	350.8	0.0000	1.6099	0.00000	0.0000
200.00	280	.0000	13.431	0.0000	362.6	0.0000	1.5951	0.00000	0.0000
400.00	230	.0000	21.488	0.0000	372.0	0.0000	1.5573	0.00000	0.0000
1000.00	175	.0000	39.928	0.0000	381.6	0.0000	1.4871	0.00000	0.0000
2000.00	142	.0000	63.572	0.0000	387.2	0.0000	1.4402	0.00000	0.0000
4000.00	114	.0000	100.939	0.0000	391.6	0.0000	1.4116	0.00000	0.0000
$R = 0.20$, PERCENT FUEL = 38.65, O/F = 1.587									
1.00	1514	0.0000							
1.05	1497	.0000	2.233	0.0000	49.3	0.0000	1.6194	0.00000	-0.0001
1.20	1450	.0000	1.289	0.0000	94.6	0.0000	1.6028	0.00000	0.0000
1.40	1398	.0000	1.077	0.0000	127.4	0.0000	1.5891	0.00000	0.0000
1.60	1354	.0000	1.016	0.0000	149.4	0.0000	1.5774	0.00000	0.0000
1.85	1307	.0000	1.000	0.0000	165.2	0.0000	1.5653	0.00000	0.0000
2.00	1282	.0000	1.004	0.0000	179.1	0.0000	1.5585	0.00000	0.0000
4.00	1079	.0000	1.244	0.0000	243.2	0.0000	1.5046	0.00000	0.0000
4.08	1073	.0000	1.256	0.0000	244.7	0.0000	1.5031	0.00000	0.0000
10.00	852	.0000	2.009	0.0000	297.2	0.0000	1.4516	0.00000	0.0000
20.00	709	.0000	3.049	0.0000	325.9	0.0000	1.4232	0.00000	0.0000
40.00	588	.0000	4.739	0.0000	348.0	0.0000	1.4067	0.00000	0.0000
100.00	458	.0000	8.679	0.0000	370.0	0.0000	1.3916	0.00000	0.0000
200.00	379	.0000	13.870	0.0000	382.7	0.0000	1.3807	0.00000	0.0000
400.00	312	.0000	22.296	0.0000	393.0	0.0000	1.3681	0.00000	0.0000
1000.00	242	.0000	41.979	0.0000	403.5	0.0000	1.3398	0.00000	0.0000
2000.00	198	.0000	67.687	0.0000	409.7	0.0000	1.2994	0.00000	0.0000
4000.00	161	.0000	108.755	0.0000	414.6	0.0000	1.2564	0.00000	0.0000
$R = 0.25$, PERCENT FUEL = 33.51, O/F = 1.984									
1.00	1816	0.0003							
1.05	1797	.0003	2.218	0.0001	50.3	0.0001	1.5988	0.00004	-0.0013
1.20	1744	.0002	1.283	0.0001	96.6	0.0001	1.5036	0.00004	-0.0012
1.40	1686	.0001	1.073	0.0000	130.1	0.0001	1.4898	0.00003	-0.0008
1.60	1636	.0001	1.015	0.0000	152.6	0.0001	1.4751	0.00002	-0.0005
1.83	1587	.0000	1.000	0.0000	171.8	0.0001	1.4630	0.00001	-0.0004
2.00	1555	.0000	1.005	0.0000	183.1	0.0001	1.4436	0.00001	-0.0002
4.00	1322	.0000	1.256	0.0000	249.3	0.0000	1.3875	0.00000	0.0000
4.08	1316	.0000	1.268	0.0000	250.8	0.0000	1.3860	0.00000	0.0000
10.00	1057	.0000	2.048	0.0000	305.6	0.0000	1.3226	0.00000	0.0000
20.00	887	.0000	3.127	0.0000	335.7	0.0000	1.2848	0.00000	0.0000
40.00	741	.0000	4.883	0.0000	359.0	0.0000	1.2559	0.00000	0.0000
100.00	581	.0000	8.985	0.0000	382.4	0.0000	1.2321	0.00000	0.0000
200.00	482	.0000	14.396	0.0000	395.9	0.0000	1.2190	0.00000	0.0000
400.00	399	.0000	23.208	0.0000	406.8	0.0000	1.2100	0.00000	0.0000
1000.00	310	.0000	43.894	0.0000	418.1	0.0000	1.1943	0.00000	0.0000
2000.00	256	.0000	71.279	0.0000	426.7	0.0000	1.1803	0.00000	0.0000
4000.00	210	.0000	115.650	0.0000	430.2	0.0000	1.1487	0.00000	0.0000
$R = 0.30$, PERCENT FUEL = 29.57, O/F = 2.381									
1.00	2089	0.0017							
1.05	2069	.0015	2.204	0.0007	50.7	0.0007	1.4493	0.00028	-0.0076
1.20	2013	.0011	1.277	0.0004	97.4	0.0006	1.4276	0.00021	-0.0077
1.40	1950	.0008	1.070	0.0002	131.3	0.0002	1.4052	0.00015	-0.0041
1.60	1896	.0005	1.013	0.0001	154.1	0.0004	1.3879	0.00010	-0.0030
1.82	1846	.0004	1.000	0.0000	172.5	0.0004	1.3729	0.00007	-0.0022
2.00	1808	.0003	1.006	-0.0001	185.1	0.0003	1.3623	0.00006	-0.0017
4.00	1553	-0.0001	1.266	-0.0002	252.5	0.0002	1.3008	0.00001	-0.0002
4.08	1546	-0.0001	1.278	-0.0002	254.1	0.0002	1.2992	0.00001	-0.0002
10.00	1258	-0.0001	2.085	-0.0002	310.4	0.0001	1.2337	0.00000	0.0000
20.00	1044	-0.0002	3.207	-0.0001	341.6	0.0001	1.1891	0.00000	0.0000
40.00	896	-0.0002	5.038	-0.0001	365.9	0.0001	1.1531	0.00000	0.0000
100.00	708	-0.0002	9.326	-0.0001	390.5	0.0000	1.1174	0.00000	0.0000
200.00	590	-0.0002	14.995	-0.0001	404.8	0.0000	1.1066	0.00000	0.0000
400.00	490	-0.0002	24.237	-0.0001	416.5	0.0000	1.0867	0.00000	0.0000
1000.00	383	-0.0002	46.005	-0.0001	428.3	0.0000	1.0745	0.00000	0.0000
2000.00	317	-0.0002	74.922	-0.0001	435.4	0.0000	1.0643	0.00000	0.0000
4000.00	262	-0.0002	122.202	-0.0001	441.2	0.0000	1.0526	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T , °K	Temperature exponent, n_T	Area ratio, ϵ	Area ratio exponent, n_ϵ	Specific impulse, I , (lbsec/lb)	Specific impulse exponent, n_I	Specific heat, c_p , cal/(g·°K)	$(\partial \ln \frac{R}{P})_T$	$(\partial \ln \frac{R}{P})_P$
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778									
1.00	2329	+0.0052						1.4897	0.00122
1.05	2309	+0.0048	2.189	0.0016	50.7	0.0020	1.4752	+0.0112	-0.0273
1.20	2253	+0.0039	1.270	+0.0012	97.5	+0.0018	1.4382	+0.0089	-0.0220
1.40	2189	+0.0030	1.067	+0.0007	131.5	+0.0016	1.3999	+0.0067	-0.0170
1.60	2133	+0.0023	1.012	+0.0003	154.4	+0.0014	1.3707	+0.0051	-0.0134
1.80	2085	+0.0018	1.000	+0.0000	171.8	+0.0013	1.3475	+0.0040	-0.0107
2.00	2042	+0.0014	1.007	+0.0002	185.6	+0.0012	1.3289	+0.0032	-0.0087
4.00	1772	+0.0001	1.277	+0.0012	253.8	+0.0007	1.2391	+0.0006	+0.0018
4.08	1764	+0.0001	1.289	+0.0010	255.4	+0.0007	1.2371	+0.0005	+0.0017
10.00	1452	+0.0005	2.121	+0.0010	312.8	+0.0004	1.1665	+0.0000	+0.0001
20.00	1239	+0.0006	3.285	+0.0009	345.0	+0.0004	1.1208	+0.0000	+0.0000
40.00	1051	+0.0006	5.194	+0.0009	370.1	+0.0004	1.0795	+0.0000	+0.0000
100.00	838	+0.0006	9.687	+0.0008	395.7	+0.0004	1.0366	+0.0000	+0.0000
200.00	703	+0.0006	15.643	+0.0008	410.7	+0.0004	1.0120	+0.0000	+0.0000
400.00	587	+0.0006	25.377	+0.0008	422.9	+0.0004	0.9954	+0.0000	+0.0000
1000.00	460	+0.0007	48.339	+0.0008	435.5	+0.0004	0.9790	+0.0000	+0.0000
2000.00	382	+0.0007	78.934	+0.0008	443.0	+0.0004	0.9694	+0.0000	+0.0000
4000.00	317	+0.0007	129.084	+0.0008	449.2	+0.0004	0.9600	+0.0000	+0.0000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175									
1.00	2531	+0.0105	2.173	+0.0029	50.4	+0.0035	1.6075	0.00316	-0.0710
1.05	2512	+0.0100	1.263	+0.0021	96.9	+0.0033	1.5870	+0.00296	-0.0671
1.20	2458	+0.0086	1.263	+0.0012	130.8	+0.0034	1.5334	+0.00248	-0.0571
1.40	2396	+0.0071	1.053	+0.0012	153.8	+0.0033	1.4758	+0.00198	-0.0465
1.60	2342	+0.0059	1.010	+0.0005	169.9	+0.0033	1.4300	+0.00162	-0.0390
1.78	2298	+0.0050	1.000	+0.0000	184.9	+0.0028	1.3954	+0.00136	-0.0332
2.00	2252	+0.0041	1.008	+0.0005	184.9	+0.0028	1.3620	+0.00112	-0.0279
4.00	1978	+0.0004	1.289	+0.0026	253.7	+0.0014	1.2167	+0.00028	-0.0079
4.08	1970	+0.0004	1.302	+0.0026	255.4	+0.0014	1.2116	+0.00027	-0.0076
10.00	1640	+0.0011	2.160	+0.0031	313.6	+0.001	1.1161	+0.00003	-0.0009
20.00	1411	+0.0014	3.365	+0.0030	346.5	+0.0004	1.0681	+0.00000	-0.0001
40.00	1207	+0.0015	5.356	+0.0029	372.4	+0.0004	1.0259	+0.00000	+0.0000
100.00	972	+0.0015	10.058	+0.0026	398.9	+0.0004	0.9772	+0.00000	+0.0000
200.00	820	+0.0016	16.345	+0.0028	414.5	+0.0004	0.9481	+0.00000	+0.0000
400.00	689	+0.0016	26.628	+0.0027	427.3	+0.0004	0.9252	+0.00000	+0.0000
1000.00	543	+0.0017	50.955	+0.0027	440.6	+0.0004	0.9041	+0.00000	+0.0000
2000.00	453	+0.0017	83.421	+0.0027	448.5	+0.0004	0.8930	+0.00000	+0.0000
4000.00	377	+0.0017	136.777	+0.0027	455.1	+0.0004	0.8834	+0.00000	+0.0000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571									
1.00	2696	+0.0164						1.7899	0.00627
1.05	2678	+0.0158	2.159	0.0033	49.9	0.0064	1.7649	+0.00597	-0.1286
1.20	2628	+0.0143	1.257	+0.0025	96.0	+0.0054	1.6982	+0.00519	-0.1137
1.40	2570	+0.0126	1.060	+0.0015	129.6	+0.0055	1.6247	+0.00438	-0.0977
1.60	2519	+0.0111	1.009	+0.0006	152.4	+0.0055	1.5642	+0.00374	-0.0849
1.77	2481	+0.0100	1.000	+0.0000	161.2	+0.0054	1.5208	+0.00330	-0.0759
2.00	2434	+0.0087	1.010	+0.0008	183.5	+0.004	1.4702	+0.00281	-0.0657
4.00	2167	+0.0024	1.303	+0.0044	252.4	+0.003	1.2440	+0.00095	-0.0246
4.08	2159	+0.0023	1.316	+0.0045	254.0	+0.003	1.2389	+0.00091	-0.0237
10.00	1822	+0.0016	2.204	+0.0064	313.0	+0.002	1.0871	+0.00013	-0.0040
20.00	1581	+0.0025	3.454	+0.0066	346.5	+0.001	1.0282	+0.00002	-0.0006
40.00	1362	+0.0027	5.529	+0.0064	373.1	+0.001	0.9843	+0.00000	-0.0001
100.00	1109	+0.0029	10.479	+0.0062	400.5	+0.000	0.9335	+0.00000	+0.0000
200.00	942	+0.0030	17.107	+0.0061	416.8	+0.000	0.9005	+0.00000	+0.0000
400.00	796	+0.0031	28.011	+0.0061	430.1	+0.000	0.8733	+0.00000	+0.0000
1000.00	632	+0.0032	53.887	+0.0061	444.1	+0.000	0.8469	+0.00000	+0.0000
2000.00	529	+0.0033	88.516	+0.0061	452.5	+0.000	0.8317	+0.00000	+0.0000
4000.00	441	+0.0033	165.512	+0.0060	459.4	+0.000	0.8212	+0.00000	+0.0000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968									
1.00	2828	+0.0218						2.0170	0.01049
1.05	2811	+0.0213	2.147	0.0033	49.2	+0.007	1.9891	+0.01009	-0.2101
1.20	2765	+0.0198	1.251	+0.0024	94.7	+0.007	1.9138	+0.00904	-0.1908
1.40	2711	+0.0181	1.057	+0.0015	128.0	+0.007	1.8487	+0.00749	-0.1696
1.60	2664	+0.0166	1.008	+0.0006	150.6	+0.007	1.7711	+0.00647	-0.1540
1.76	2632	+0.0156	1.000	+0.0000	164.2	+0.006	1.7087	+0.00637	-0.1403
2.00	2585	+0.0140	1.012	+0.0009	181.4	+0.006	1.6426	+0.00557	-0.1247
4.00	2335	+0.0062	1.317	+0.0055	250.2	+0.005	1.3401	+0.00237	-0.0580
4.08	2327	+0.0060	1.331	+0.0056	251.6	+0.005	1.3326	+0.00230	-0.0565
10.00	1996	+0.0012	2.252	+0.0097	311.3	+0.003	1.0939	+0.00048	-0.0135
20.00	1748	+0.0035	3.552	+0.0107	345.4	+0.002	1.0036	+0.00009	-0.0030
40.00	1518	+0.0043	5.719	+0.0107	372.6	+0.002	0.9523	+0.00001	-0.0004
100.00	1247	+0.0046	10.920	+0.0105	400.8	+0.001	0.9003	+0.00000	+0.0000
200.00	1067	+0.0048	17.932	+0.0104	417.7	+0.001	0.8650	+0.00000	+0.0000
400.00	907	+0.0050	29.520	+0.0103	431.6	+0.001	0.8347	+0.00000	+0.0000
1000.00	727	+0.0052	57.146	+0.0103	446.3	+0.000	0.8023	+0.00000	+0.0000
2000.00	611	+0.0053	94.228	+0.0103	455.1	+0.000	0.7848	+0.00000	+0.0000
4000.00	512	+0.0054	155.405	+0.0103	462.4	+0.000	0.7703	+0.00000	+0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIO SURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T_c , K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I , lb/(sec·lb)	Specific-impulse exponent, n_I	Specific heat, $c_d/(g_m^{\text{ideal}})$	$(\frac{\partial \ln I}{\partial \ln P})_T$	$(\frac{\partial \ln I}{\partial \ln T})_P$
$R = 0.60, \text{ PERCENT FUEL} = 17.35, \text{ O/F} = 4.762$									
1.00	3015	0.0304	2.131	0.0026	47.7	0.0103	2.5641	0.02196	-0.4374
1.05	3001	0.0300	1.244	0.0020	91.9	0.0106	2.5343	0.02139	-0.4278
1.20	2961	0.0288	1.054	0.0012	124.4	0.0103	2.4522	0.01985	-0.3722
1.40	2914	0.0274	1.006	0.0005	146.2	0.0101	2.3566	0.01813	-0.3469
1.60	2874	0.0262	1.000	0.0000	158.0	0.0100	2.2225	0.01668	-0.3315
1.74	2849	0.0254	1.014	-0.0002	176.3	0.0097	2.1550	0.01439	-0.3053
2.00	2807	0.0240	1.339	-0.0002	244.1	0.0085	1.7214	0.00832	-0.1889
4.00	2595	0.0165	1.354	-0.0054	245.7	0.0084	1.7099	0.00816	-0.1858
4.08	2588	0.0162							
10.00	2299	0.0053	2.346	-0.0120	302.5	0.0067	1.7736	0.00301	-0.0756
20.00	2063	-0.0021	3.762	-0.0165	340.5	0.0024	1.0527	0.00101	-0.0278
40.00	1825	-0.0064	6.136	-0.0189	368.8	0.0044	0.9310	0.00024	-0.0074
100.00	1529	-0.0084	11.885	-0.0195	398.6	0.0020	0.8551	0.00002	-0.0007
200.00	1326	-0.0094	19.472	-0.0193	416.6	0.0024	0.8176		-0.0001
400.00	1144	-0.0093	32.844	-0.0192	431.6	0.0019	0.7842		0.0000
1000.00	932	-0.0098	64.475	-0.0193	447.7	0.0015	0.7449		0.0000
2000.00	792	-0.0101	107.316	-0.0193	457.5	0.0012	0.7201		0.0000
4000.00	670	-0.0104	178.419	-0.0194	465.6	0.0010	0.7001		0.0000
$R = 0.70, \text{ PERCENT FUEL} = 15.25, \text{ O/F} = 5.556$									
1.00	3128	0.0362	2.122	0.0020	46.1	0.0126	3.1609	0.03650	-0.7110
1.05	3114	0.0358	1.240	0.0015	88.9	0.0129	3.1356	0.03584	-0.7011
1.20	3078	0.0349	1.051	0.0009	120.2	0.0123	3.0846	0.03406	-0.6738
1.40	3037	0.0339	1.005	0.0003	141.5	0.0121	2.9793	0.03201	-0.6417
1.60	3001	0.0329	1.000	-0.0003	152.2	0.0120	2.8581	0.03026	-0.6135
1.73	2981	0.0324	1.000	-0.0000	152.2	0.0118	2.7698	0.02738	-0.5657
2.00	2943	0.0313	1.015	-0.0006	170.8	0.0116	2.6362	0.01894	-0.4182
4.00	2761	0.0255	1.353	-0.0040	237.0	0.0108	2.3126	0.01070	-0.1020
4.08	2756	0.0254	1.369	-0.0041	238.6	0.0108	0.1870		
10.00	2517	0.0160	2.441	-0.0099	297.8	0.0094	1.7290	0.00970	-0.2309
20.00	2320	-0.0071	5.943	-0.0155	333.0	0.0084	1.3390	0.00478	-0.1218
40.00	2108	-0.0021	6.551	-0.0215	362.1	0.0069	1.0559	0.00183	-0.0505
100.00	1813	-0.0103	12.932	-0.0265	395.3	0.0053	0.8583	0.00031	-0.0098
200.00	1596	-0.0127	21.699	-0.0276	412.5	0.0044	0.7942	0.00005	-0.0019
400.00	1395	-0.0137	36.494	-0.0277	428.6	0.0034	0.7553	0.00001	-0.0002
1000.00	1156	-0.0146	72.660	-0.0277	446.0	0.0026	0.7136		0.0000
2000.00	990	-0.0152	122.229	-0.0279	456.0	0.0022	0.6848		0.0000
4000.00	853	-0.0158	205.254	-0.0281	465.9	0.0018	0.6596		0.0000
$R = 0.80, \text{ PERCENT FUEL} = 13.60, \text{ O/F} = 6.349$									
1.00	3188	0.0395	2.117	0.0016	44.6	0.0136	3.6135	0.05035	-0.9676
1.05	3175	0.0392	1.238	0.0012	86.0	0.0135	3.5978	0.04974	-0.9597
1.20	3141	0.0385	1.050	0.0007	115.3	0.0134	3.5527	0.04808	-0.9377
1.40	3103	0.0377	1.005	0.0002	137.0	0.0132	3.4973	0.04616	-0.9115
1.60	3070	0.0370	1.005	0.0002	147.0	0.0131	3.4461	0.04449	-0.8880
1.72	3052	0.0366	1.000	-0.0000	147.0	0.0130	3.4169	0.04357	-0.8746
2.00	3016	0.0358	1.016	-0.0003	165.3	0.0130	3.3594	0.04169	-0.8472
4.00	2853	0.0317	1.361	-0.0030	229.7	0.0122	3.0181	0.03300	-0.7089
4.08	2848	0.0316	1.376	-0.0030	231.2	0.0122	3.0070	0.03275	-0.7046
10.00	2645	0.0252	2.453	-0.0069	289.2	0.0114	2.4611	0.02178	-0.5040
20.00	2487	0.0188	4.060	-0.0110	324.1	0.0103	1.9810	0.01399	-0.3434
40.00	2321	-0.0102	6.873	-0.0166	353.4	0.0093	1.5084	0.00757	-0.1977
100.00	2074	-0.0038	13.944	-0.0261	385.5	0.0078	1.0340	0.00229	-0.0656
200.00	1868	-0.0125	23.785	-0.0319	402.7	0.0062	0.8617	0.00065	-0.0204
400.00	1658	-0.0170	40.475	-0.0345	422.9	0.0054	0.7527	0.00013	-0.0044
1000.00	1398	-0.0191	81.680	-0.0353	441.8	0.0042	0.6975		0.0000
2000.00	1220	-0.0201	138.794	-0.0355	453.6	0.0035	0.6676		0.0000
4000.00	1058	-0.0210	235.555	-0.0358	463.7	0.0029	0.6395		0.0000
$R = 0.90, \text{ PERCENT FUEL} = 12.25, \text{ O/F} = 7.143$									
1.00	3213	0.0410	2.115	0.0014	43.2	0.0141	3.7584	0.05880	-1.1225
1.05	3201	0.0408	1.215	0.0012	83.2	0.0139	3.7253	0.05821	-1.1167
1.20	3168	0.0401	1.238	0.0010	112.6	0.0138	3.6942	0.05683	-1.1040
1.40	3131	0.0394	1.050	0.0005	132.7	0.0137	3.6652	0.05515	-1.0869
1.60	3099	0.0388	1.005	0.0002	142.7	0.0136	3.6365	0.05371	-1.0653
1.72	3082	0.0385	1.000	-0.0000	142.7	0.0136	3.6047	0.05293	-1.0538
2.00	3047	0.0378	1.017	-0.0004	160.4	0.0134	3.5612	0.05129	-1.0332
4.00	2892	0.0346	1.364	-0.0024	222.6	0.0128	3.0412	0.04380	-0.9301
4.08	2888	0.0345	1.379	-0.0025	224.1	0.0128	3.0409	0.04358	-0.9269
10.00	2701	0.0300	2.470	-0.0053	280.5	0.0120	2.0504	0.03399	-0.7736
20.00	2564	0.0261	4.112	-0.0077	314.6	0.0113	2.7328	0.02668	-0.6403
40.00	2429	0.0214	7.032	-0.0107	343.6	0.0107	2.3391	0.01951	-0.4967
100.00	2246	0.0125	14.621	-0.0166	375.8	0.0097	1.7259	0.01052	-0.4887
200.00	2095	0.0119	25.591	-0.0241	396.6	0.0088	1.4476	0.00487	-0.1433
400.00	1919	-0.0112	44.582	-0.0335	414.7	0.0077	0.8980	0.0150	-0.0477
1000.00	1660	-0.0216	91.675	-0.0406	435.1	0.0064	0.7114	0.00018	-0.0064
2000.00	1468	-0.0442	157.405	-0.0520	448.0	0.0052	0.6631	0.0003	-0.0101
4000.00	1289	-0.0256	269.819	-0.0424	459.1	0.0043	0.5235		0.0001

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T , °K	Temperature exponent, n_1	Area ratio, ϵ	Area-ratio exponent, n_2	Specific impulse, I , (lb)(sec./lb)	Specific-impulse exponent, n_3	Specific heat, c_p , cal/(g·°K)	$(\frac{\partial \ln R}{\partial \ln P})_T$	$(\frac{\partial \ln R}{\partial \ln T})_P$
$R = 1.00$, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3217	0.0412					3.6327	0.06081	-1.1607
1.05	3205	-0.010	2.115	0.0014	41.9	0.0141	3.6262	-0.0631	-1.1555
1.20	3173	0.040	1.237	0.010	80.8	0.0140	3.6075	-0.0584	-1.1409
1.40	3136	0.039	1.050	0.006	109.3	0.0138	3.5839	-0.05736	-1.1235
1.60	3104	0.0391	1.005	0.002	128.7	0.0137	3.5618	-0.05599	-1.1080
1.72	3088	0.0388	1.000	0.000	137.9	0.0136	3.5493	-0.05546	-1.0955
2.00	3053	0.0382	1.017	-0.004	155.4	0.0135	3.5214	-0.05371	-1.0811
4.00	2900	0.0351	1.364	-0.023	216.0	0.0129	3.3663	-0.04671	-0.9903
4.08	2896	0.0350	1.380	-0.024	217.5	0.0129	3.3631	-0.04650	-0.9874
10.00	2713	0.0310	2.474	-0.049	272.3	0.0121	3.1047	-0.03772	-0.8556
20.00	2579	0.0277	4.124	-0.070	305.6	0.0115	2.8627	-0.03120	-0.7448
40.00	2452	0.0242	7.068	-0.092	333.7	0.0109	2.5882	-0.02502	-0.6289
100.00	2287	0.0187	14.785	-0.127	365.2	0.0101	2.1850	-0.01751	-0.4723
200.00	2164	0.0137	26.152	-0.160	385.7	0.0095	1.8612	-0.01248	-0.3562
400.00	2037	0.0075	46.510	-0.202	403.9	0.0089	1.5363	-0.00816	-0.2476
1000.00	1859	-0.0050	99.697	-0.277	424.9	0.0079	1.1390	-0.00380	-0.1267
2000.00	1710	-0.0127	176.636	-0.348	438.8	0.0070	0.8974	-0.00170	-0.0615
4000.00	1549	-0.0219	310.311	-0.417	451.0	0.0061	0.7318	-0.00058	-0.0230
$R = 1.50$, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3116	0.0362					2.2973	0.03957	-0.7944
1.15	3103	0.0359	2.117	0.0016	37.2	0.0126	2.2869	0.03905	-0.7873
1.20	3070	0.0352	1.238	0.012	71.6	0.0125	2.2574	0.03763	-0.7675
1.40	3031	0.034	1.050	0.007	96.8	0.0123	2.2216	0.03601	-0.7443
1.60	2999	0.036	1.005	0.002	114.1	0.0122	2.1892	0.03461	-0.7238
1.72	2981	0.0352	1.000	0.000	122.4	0.0121	2.1710	0.03385	-0.7124
2.00	2945	0.0324	1.018	-0.003	137.7	0.0120	2.1323	0.03230	-0.6887
4.00	2782	0.0284	1.361	-0.029	191.3	0.0112	1.9340	0.02538	-0.5752
4.08	2777	0.0282	1.377	-0.030	192.6	0.0112	1.9277	0.02518	-0.5717
10.00	2576	0.0223	2.454	-0.065	240.8	0.0102	1.6300	-0.01698	-0.4190
20.00	2421	0.0168	4.065	-0.099	270.0	0.0094	1.3799	-0.01144	-0.3029
40.00	2263	0.0102	6.896	-0.141	294.4	0.0086	1.1285	-0.00685	-0.1965
100.00	2040	-0.0003	14.098	-0.212	321.3	0.0073	0.8344	-0.00264	-0.0862
200.00	1856	-0.0082	24.259	-0.267	338.4	0.0063	0.6739	-0.00096	-0.0355
400.00	1664	-0.0139	41.606	-0.306	353.1	0.0053	0.5774	-0.00026	-0.0112
1000.00	1415	-0.0175	84.484	-0.326	369.3	0.0041	0.5156	-0.00003	-0.0017
2000.00	1240	-0.0187	144.082	-0.331	379.5	0.0034	0.4898	-0.00000	-0.0003
4000.00	1080	-0.0196	245.360	-0.334	388.2	0.0029	0.4690	-0.00000	-0.0000
$R = 2.00$, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	2966	0.0297					1.5209	0.02254	-0.4874
1.05	2953	0.029	2.122	0.0019	34.1	0.0107	1.5098	0.02210	-0.4802
1.20	2917	0.0285	1.240	0.014	65.7	0.0106	1.4788	0.02091	-0.4605
1.40	2877	0.0275	1.052	0.008	88.8	0.0104	1.4419	0.01957	-0.4376
1.60	2841	0.0266	1.005	0.003	104.6	0.0102	1.4091	0.01842	-0.4178
1.72	2821	0.0260	1.000	0.000	112.6	0.0101	1.3901	0.01778	-0.4064
2.00	2783	0.0250	1.015	-0.006	126.3	0.0099	1.3529	0.01657	-0.3846
4.00	2604	0.0197	1.353	-0.037	175.2	0.0090	1.1688	0.01130	-0.2831
4.08	2599	0.0196	1.368	-0.038	176.4	0.0090	1.1632	0.01116	-0.2802
10.00	2365	0.0117	2.412	-0.087	220.1	0.0078	0.9205	-0.00575	-0.1616
20.00	2177	0.0048	3.941	-0.131	246.1	0.0067	0.7501	-0.00286	-0.0890
40.00	1978	-0.0019	6.557	-0.175	267.6	0.0056	0.6166	-0.00114	-0.0400
100.00	1706	-0.0080	12.980	-0.214	296.7	0.0043	0.5100	-0.00022	-0.0096
200.00	1505	-0.0102	21.822	-0.224	305.0	0.0035	0.4679	-0.00005	-0.0024
400.00	1318	-0.0111	36.754	-0.227	316.9	0.0029	0.4457	-0.00001	-0.0005
1000.00	1095	-0.0118	73.335	-0.227	329.9	0.0022	0.4221	-0.00000	-0.0000
2000.00	945	-0.0123	123.637	-0.228	338.0	0.0018	0.4064	-0.00000	-0.0000
4000.00	812	-0.0128	208.163	-0.230	344.8	0.0015	0.3916	-0.00000	-0.0000
$R = 3.00$, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2655	0.0175					0.8140	0.00697	-0.1761
1.05	2640	0.0171	2.140	0.0026	30.2	0.0067	0.8048	0.00672	-0.1708
1.20	2599	0.0160	1.248	0.019	58.1	0.0065	0.7795	0.00604	-0.1566
1.40	2550	0.0147	1.056	0.011	78.5	0.0063	0.7506	0.00531	-0.1404
1.60	2509	0.0135	1.007	0.005	92.3	0.0061	0.7260	0.00472	-0.1276
1.72	2481	0.0127	1.000	0.000	100.3	0.0059	0.7099	0.00435	-0.1193
2.00	2438	0.0116	1.013	-0.007	111.3	0.0057	0.6858	0.00382	-0.1070
4.00	2216	0.0057	1.325	-0.043	153.7	0.0046	0.5739	0.00175	-0.0590
4.08	2209	0.0055	1.339	-0.044	154.8	0.0045	0.5710	0.00170	-0.0538
10.00	1915	-0.0002	2.286	-0.079	191.7	0.0032	0.4712	-0.00044	-0.0165
20.00	1691	-0.0026	3.629	-0.092	213.1	0.0024	0.4277	-0.00011	-0.0050
40.00	1480	-0.0036	5.877	-0.095	230.2	0.0019	0.4030	-0.00002	-0.0012
100.00	1229	-0.0040	11.319	-0.093	248.1	0.0013	0.3820	-0.00000	-0.0001
200.00	1061	-0.0042	18.732	-0.092	258.9	0.0011	0.3686	-0.00000	-0.0000
400.00	911	-0.0043	31.103	-0.092	267.9	0.0009	0.3561	-0.00000	-0.0000
1000.00	739	-0.0045	60.907	-0.092	277.4	0.0006	0.3403	-0.00000	-0.0000
2000.00	627	-0.0047	101.211	-0.094	283.3	0.0005	0.3295	-0.00000	-0.0000
4000.00	529	-0.0044	167.921	-0.094	286.1	0.0004	0.3198	-0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_1	Area ratio, ϵ	Area-ratio exponent, n_2	Specific impulse, I, (lb/sec)/lb	Specific-impulse exponent, n_3	Specific heat, c_p , cal/(lb·°F)	$(\frac{\partial \ln M}{\partial \ln P})_T$	$(\frac{\partial \ln M}{\partial \ln T})_P$
$R = 4.00, \text{ PERCENT FUEL} = 3.05, \text{ O/F} = 1.746$									
1.00	2347	0.0079					0.5285	0.00185	-0.0552
1.05	2330	0.0075	2.165	0.0021	27.4	0.0032	.5227	0.00175	-0.0525
1.20	2282	0.0066	1.260	0.0015	52.7	0.0030	.5073	0.00147	-0.0454
1.40	2228	0.0056	1.061	0.0009	71.2	0.0028	.4906	0.00120	-0.0380
1.60	2180	0.0047	1.009	0.0004	83.6	0.0026	.4772	0.00099	-0.0323
1.78	2143	0.0041	1.000	0.0000	92.1	0.0024	.4674	0.00085	-0.0283
2.00	2101	0.0034	1.009	-0.0004	100.7	0.0023	.4569	0.00071	-0.0242
4.00	1858	0.0006	1.297	-0.0021	138.3	0.0016	.4102	0.00021	-0.0084
4.08	1851	0.0006	1.311	-0.0021	135.2	0.0016	.4092	0.00020	-0.0082
10.00	1556	-0.0008	2.192	-0.0027	171.3	0.0010	.3769	0.00003	-0.0015
20.00	1351	-0.0011	3.439	-0.0027	189.6	0.0007	.3619	0.00000	-0.0003
40.00	1167	-0.0012	5.518	-0.0027	204.1	0.0005	.3501	0.00000	-0.0000
100.00	954	-0.0013	10.507	-0.0026	219.1	0.0004	.3354	0.00000	-0.0000
200.00	815	-0.0013	17.236	-0.0025	228.0	0.0003	.3244	0.00000	-0.0000
400.00	692	-0.0014	28.356	-0.0025	235.4	0.0002	.3141	0.00000	-0.0000
1000.00	553	-0.0014	54.842	-0.0025	243.2	0.0002	.3013	0.00000	-0.0000
2000.00	464	-0.0015	90.278	-0.0025	247.9	0.0001	.2929	0.00000	-0.0000
4000.00	387	-0.0015	148.471	-0.0025	251.7	0.0001	.2865	0.00000	-0.0000
$R = 5.00, \text{ PERCENT FUEL} = 2.45, \text{ O/F} = 9.683$									
1.00	2062	0.0027					0.4109	0.00043	-0.0153
1.05	2044	0.0025	2.186	0.0010	25.2	0.0011	.4079	0.00040	-0.0142
1.20	1995	0.0020	1.269	0.0007	48.4	0.0010	.4004	0.00032	-0.0116
1.40	1938	0.0016	1.066	0.0004	65.3	0.0009	.3925	0.00024	-0.0091
1.60	1890	0.0012	1.011	0.0002	76.7	0.0008	.3864	0.00019	-0.0073
1.80	1849	0.0010	1.000	0.0000	85.1	0.0008	.3816	0.00015	-0.0060
2.00	1811	0.0008	1.007	-0.0001	92.2	0.0007	.3775	0.00012	-0.0050
4.00	1578	0.0000	1.282	-0.0005	126.2	0.0004	.3579	0.00003	-0.0013
4.08	1571	0.0000	1.295	-0.0005	127.0	0.0004	.3575	0.00002	-0.0012
10.00	1304	-0.0003	2.145	-0.0006	155.7	0.0002	.3413	0.00000	-0.0001
20.00	1122	-0.0003	3.345	-0.0006	171.9	0.0002	.3309	0.00000	-0.0000
40.00	961	-0.0003	5.334	-0.0005	184.7	0.0001	.3209	0.00000	-0.0000
100.00	778	-0.0003	10.072	-0.0005	197.8	0.0001	.3076	0.00000	-0.0000
200.00	659	-0.0004	16.410	-0.0005	205.6	0.0001	.2979	0.00000	-0.0000
400.00	555	-0.0004	26.810	-0.0005	212.0	0.0001	.2888	0.00000	-0.0000
1000.00	438	-0.0004	51.370	-0.0005	218.6	0.0000	.2783	0.00000	-0.0000
2000.00	365	-0.0004	84.029	-0.0005	222.6	0.0000	.2728	0.00000	-0.0000
4000.00	303	-0.0004	137.526	-0.0005	225.9	0.0000	.2693	0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, $T, ^\circ K$	Temperature exponent, η_1	Area ratio, ϵ	Area-ratio exponent, η_2	Specific impulse, $I, (lb/sec)/lb$	Specific-impulse exponent, η_3	Specific heat, $c_p, \text{cal}/(\text{lb}^\circ \text{K})$	$(\frac{\partial \ln M}{\partial \ln P})_T$	$(\frac{\partial \ln M}{\partial \ln T})_P$
$R = 0.15, \text{ PERCENT FUEL} = 45.65, \text{ O/F} = 1.190$									
1.00	1183	0.0000						1.7752	0.00000
1.05	1168	0.0000	2.250	0.0000	47.4	0.0000	1.7711	0.00000	0.0000
1.20	1129	0.0000	1.297	0.0000	90.8	0.0000	1.7597	0.00000	0.0000
1.40	1085	0.0000	1.081	0.0000	122.2	0.0000	1.7473	0.00000	0.0000
1.60	1049	0.0000	1.018	0.0000	143.2	0.0000	1.7368	0.00000	0.0000
1.87	1008	0.0000	1.000	0.0000	163.4	0.0000	1.7257	0.00000	0.0000
2.00	989	0.0000	1.003	0.0000	171.5	0.0000	1.7210	0.00000	0.0000
4.00	824	0.0000	1.233	0.0000	232.3	0.0000	1.6825	0.00000	0.0000
10.00	643	0.0000	1.974	0.0000	283.1	0.0000	1.6505	0.00000	0.0000
10.21	639	0.0000	1.997	0.0000	284.0	0.0000	1.6501	0.00000	0.0000
20.00	532	0.0000	2.982	0.0000	309.9	0.0000	1.6343	0.00000	0.0000
40.00	439	0.0000	4.620	0.0000	330.4	0.0000	1.6269	0.00000	0.0000
100.00	340	0.0000	8.432	0.0000	350.8	0.0000	1.6091	0.00000	0.0000
200.00	280	0.0000	13.431	0.0000	362.6	0.0000	1.5971	0.00000	0.0000
400.00	230	0.0000	21.488	0.0000	372.0	0.0000	1.5556	0.00000	0.0000
1000.00	175	0.0000	39.928	0.0000	381.6	0.0000	1.4845	0.00000	0.0000
2000.00	142	0.0000	63.572	0.0000	387.2	0.0000	1.4387	0.00000	0.0000
4000.00	114	0.0000	100.938	0.0000	391.6	0.0000	1.4054	0.00000	0.0000
$R = 0.20, \text{ PERCENT FUEL} = 38.65, \text{ O/F} = 1.587$									
1.00	1514	0.0000						1.6191	0.00000
1.05	1497	0.0000	2.233	0.0000	49.3	0.0000	1.6146	0.00000	0.0000
1.20	1450	0.0000	1.289	0.0000	94.6	0.0000	1.6026	0.00000	0.0000
1.40	1398	0.0000	1.077	0.0000	127.4	0.0000	1.5889	0.00000	0.0000
1.60	1354	0.0000	1.016	0.0000	149.4	0.0000	1.5773	0.00000	0.0000
1.85	1307	0.0000	1.000	0.0000	169.2	0.0000	1.5652	0.00000	0.0000
2.00	1282	0.0000	1.004	0.0000	179.1	0.0000	1.5585	0.00000	0.0000
4.00	1079	0.0000	1.244	0.0000	243.2	0.0000	1.5045	0.00000	0.0000
10.00	852	0.0000	2.009	0.0000	297.2	0.0000	1.4516	0.00000	0.0000
10.21	847	0.0000	2.033	0.0000	298.2	0.0000	1.4506	0.00000	0.0000
20.00	709	0.0000	3.049	0.0000	325.9	0.0000	1.4232	0.00000	0.0000
40.00	588	0.0000	4.739	0.0000	348.0	0.0000	1.4067	0.00000	0.0000
100.00	458	0.0000	8.679	0.0000	370.0	0.0000	1.3914	0.00000	0.0000
200.00	379	0.0000	13.870	0.0000	382.7	0.0000	1.3867	0.00000	0.0000
400.00	312	0.0000	22.295	0.0000	393.0	0.0000	1.3677	0.00000	0.0000
1000.00	242	0.0000	41.979	0.0000	403.5	0.0000	1.3402	0.00000	0.0000
2000.00	198	0.0000	67.687	0.0000	409.7	0.0000	1.2958	0.00000	0.0000
4000.00	161	0.0000	108.754	0.0000	414.6	0.0000	1.2580	0.00000	0.0000
$R = 0.25, \text{ PERCENT FUEL} = 33.51, \text{ O/F} = 1.984$									
1.00	1816	0.0002						1.5040	0.00003
1.05	1797	0.0002	2.218	0.0001	50.3	0.0101	1.4992	0.00002	-0.0009
1.20	1745	0.0001	1.283	0.0001	94.6	0.01	1.4867	0.00002	-0.0005
1.40	1686	0.0001	1.073	0.0000	130.1	0.01	1.4730	0.00001	-0.0003
1.60	1636	0.0000	1.015	0.0000	152.7	0.00	1.4616	0.00001	-0.0002
1.83	1587	0.0000	1.000	0.0000	171.8	0.00	1.4503	0.00000	-0.0001
2.00	1555	0.0000	1.005	0.0000	183.1	0.00	1.4429	0.00000	-0.0001
4.00	1322	0.0000	1.256	0.0000	249.3	0.00	1.3875	0.00000	0.0000
10.00	1057	0.0000	2.048	0.0000	305.6	0.00	1.3225	0.00000	0.0000
10.21	1052	0.0000	2.073	0.0000	306.6	0.00	1.3213	0.00000	0.0000
20.00	887	0.0000	3.127	0.0000	335.7	0.00	1.2847	0.00000	0.0000
40.00	741	0.0000	4.883	0.0000	359.0	0.00	1.2559	0.00000	0.0000
100.00	581	0.0000	8.985	0.0000	382.4	0.00	1.2320	0.00000	0.0000
200.00	482	0.0000	14.396	0.0000	395.9	0.00	1.2190	0.00000	0.0000
400.00	399	0.0000	23.208	0.0000	406.8	0.00	1.2100	0.00000	0.0000
1000.00	310	0.0000	43.894	0.0000	418.1	0.00	1.1953	0.00000	0.0000
2000.00	256	0.0000	71.280	0.0000	424.7	0.00	1.1803	0.00000	0.0000
4000.00	210	0.0000	115.651	0.0000	430.2	0.00	1.1481	0.00000	0.0000
$R = 0.30, \text{ PERCENT FUEL} = 29.57, \text{ O/F} = 2.381$									
1.00	2092	0.0011						1.4348	0.00020
1.05	2071	0.0010	2.205	0.0004	50.8	0.0104	1.4282	0.00018	-0.0049
1.20	2015	0.0007	1.277	0.0003	97.5	0.0104	1.4111	0.00013	-0.0037
1.40	1951	0.0005	1.070	0.0002	131.4	0.0103	1.3931	0.00009	-0.0026
1.60	1897	0.0003	1.013	0.0001	157.2	0.0103	1.3786	0.00007	-0.0019
1.82	1846	0.0002	1.000	0.0000	172.6	0.0102	1.3659	0.00005	-0.0014
2.00	1809	0.0002	1.005	0.0000	185.1	0.0102	1.3567	0.00004	-0.0011
4.00	1553	-0.0001	1.266	-0.0001	252.5	0.0101	1.2999	0.00000	-0.0004
10.00	1258	-0.0001	2.085	-0.0001	310.4	0.0101	1.2337	0.00000	0.0000
10.21	1251	-0.0001	2.111	-0.0001	311.5	0.0101	1.2322	0.00000	0.0000
20.00	1064	-0.0001	3.206	-0.0001	341.7	0.0100	1.1891	0.00000	0.0000
40.00	895	-0.0001	5.037	-0.0001	366.0	0.0100	1.1531	0.00000	0.0000
100.00	708	-0.0001	9.325	-0.0001	390.5	0.0100	1.1175	0.00000	0.0000
200.00	590	-0.0001	14.994	-0.0001	404.8	0.0100	1.1008	0.00000	0.0000
400.00	490	-0.0001	24.235	-0.0001	416.5	0.0100	1.0868	0.00000	0.0000
1000.00	383	-0.0001	46.002	-0.0001	428.3	0.0100	1.0745	0.00000	0.0000
2000.00	317	-0.0001	74.917	-0.0001	435.4	0.0100	1.0637	0.00000	0.0000
4000.00	262	-0.0001	122.133	-0.0001	441.2	0.0100	1.0533	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area ratio exponent, n _ε	Specific impulse, I _s (lb/sec)	Specific impulse exponent, n _I	Specific heat, c _p (cal/gm°K)	(δ ln M) / (δ ln P) _T	(δ ln M) / (δ ln T) _P
<i>R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778</i>									
1.00	2339	0.0036	2.192	0.0012	50.0	0.0014	1.4471	0.00051	-0.0194
1.05	2317	0.0033	2.171	0.0009	97.0	0.0012	1.4164	0.0074	-0.0180
1.20	2259	0.0026	1.271	0.0005	131.0	0.0011	1.3889	0.0058	-0.0144
1.40	2193	0.0020	1.057	0.0005	151.0	0.0010	1.3504	0.0043	-0.0110
1.60	2137	0.0017	1.012	0.0004	154.0	0.0010	1.3385	0.0033	-0.0086
1.80	2087	0.0011	1.000	0.0004	172.1	0.0009	1.3209	0.0026	-0.0069
2.00	2044	0.0009	1.007	0.0001	165.7	0.0008	1.3068	0.0021	-0.0056
4.00	1772	-0.0001	1.276	-0.0006	254.0	0.0005	1.2337	0.0004	-0.0011
10.00	1451	-0.0003	2.120	-0.0005	312.9	0.0003	1.1659	0.0000	-0.0001
10.21	1444	-0.0003	2.147	-0.0005	314.0	0.0003	1.1645	0.0000	-0.0001
20.00	1239	-0.0004	3.282	-0.0006	345.1	0.0002	1.1206	0.0000	0.0000
40.00	1051	-0.0004	5.191	-0.0005	370.2	0.0001	1.0794	0.0000	0.0000
100.00	838	-0.0004	9.681	-0.0005	395.8	0.0001	1.0366	0.0000	0.0000
200.00	702	-0.0004	15.634	-0.0005	410.8	0.0001	1.0119	0.0000	0.0000
400.00	586	-0.0004	25.362	-0.0005	424.9	0.0001	0.9953	0.0000	0.0000
1000.00	460	-0.0004	48.312	-0.0005	435.5	0.0000	0.9789	0.0000	0.0000
2000.00	382	-0.0004	78.890	-0.0005	443.0	0.0000	0.9694	0.0000	0.0000
4000.00	317	-0.0004	129.010	-0.0005	449.2	0.0000	0.9587	0.0000	0.0000
<i>R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175</i>									
1.00	2553	0.0078	4.178	0.0042	50.6	0.0029	1.4879	0.00219	-0.0489
1.05	2532	0.0014	4.178	0.0042	50.6	0.0027	1.4725	0.00205	-0.0460
1.20	2475	0.0053	1.265	0.0116	97.2	0.0027	1.4323	0.0159	-0.0388
1.40	2410	0.0051	1.064	0.0209	131.2	0.0029	1.3894	0.0134	-0.0315
1.60	2353	0.0041	1.011	0.0094	154.1	0.0023	1.3555	0.0108	-0.0259
1.79	2306	0.0034	1.000	0.0000	170.6	0.0021	1.3293	0.0090	-0.0219
2.00	2260	0.0028	1.008	0.0004	185.5	0.0020	1.3054	0.0074	-0.0183
4.00	1978	0.0004	1.286	-0.0017	254.0	0.0013	1.1954	0.0018	-0.0050
10.00	1638	-0.0008	2.155	-0.0021	315.9	0.0007	1.1133	0.0002	-0.0005
10.21	1631	-0.0008	2.182	-0.0021	315.0	0.0007	1.1119	0.0001	-0.0005
20.00	1410	-0.0010	3.358	-0.0020	346.7	0.0005	1.0674	0.0000	-0.0001
40.00	1206	-0.0010	5.344	-0.0019	372.5	0.0004	1.0256	0.0000	-0.0007
100.00	971	-0.0011	10.047	-0.0018	399.0	0.0003	0.9769	0.0000	0.0000
200.00	819	-0.0011	16.311	-0.0018	414.6	0.0002	0.9479	0.0000	0.0000
400.00	688	-0.0011	26.573	-0.0018	427.4	0.0002	0.9251	0.0000	0.0000
1000.00	543	-0.0011	50.851	-0.0018	440.5	0.0001	0.9040	0.0000	0.0000
2000.00	452	-0.0012	85.253	-0.0018	448.5	0.0001	0.8930	0.0000	0.0000
4000.00	376	-0.0012	136.502	-0.0018	455.1	0.0001	0.8832	0.0000	0.0000
<i>R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571</i>									
1.00	2733	0.0131	4.165	0.0030	50.1	0.0048	1.4977	0.00497	-0.0965
1.05	2713	0.0126	4.165	0.0030	50.1	0.0048	1.4881	0.00433	-0.0941
1.20	2659	0.0112	1.259	0.022	96.4	0.0045	1.4361	0.0372	-0.0806
1.40	2596	0.0096	1.061	0.013	130.2	0.0042	1.4792	0.0309	-0.0684
1.60	2542	0.0085	1.009	0.0036	153.0	0.0040	1.4330	0.0261	-0.0588
1.77	2499	0.0073	1.000	0.0000	168.4	0.0038	1.3991	0.0227	-0.0519
2.00	2451	0.0063	1.009	-0.0006	184.2	0.0035	1.3621	0.0192	-0.0447
4.00	2171	0.0014	1.298	-0.0013	253.0	0.0025	1.1951	0.0081	-0.0159
10.00	1819	-0.0013	2.193	-0.0046	315.5	0.0010	1.0768	0.0008	-0.0025
10.21	1812	-0.0013	2.221	-0.0046	314.7	0.0010	1.0750	0.0008	-0.0024
20.00	1578	-0.0016	3.446	-0.0046	346.4	0.0011	1.0258	0.0001	-0.0004
40.00	1359	-0.0020	5.020	-0.0045	373.4	0.0008	0.9835	0.0000	0.0000
100.00	1108	-0.0021	10.428	-0.0042	400.7	0.0000	0.9330	0.0000	0.0000
200.00	929	-0.0022	17.026	-0.0043	417.0	0.0003	0.9001	0.0000	0.0000
400.00	794	-0.0023	27.579	-0.0043	430.2	0.0004	0.8730	0.0000	0.0000
1000.00	631	-0.0023	54.635	-0.0042	444.2	0.0003	0.8467	0.0000	0.0000
2000.00	528	-0.0024	88.103	-0.0042	452.6	0.0004	0.8316	0.0000	0.0000
4000.00	440	-0.0024	144.834	-0.0042	459.2	0.0004	0.8211	0.0000	0.0000
<i>R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968</i>									
1.00	2881	0.0185	2.153	0.0032	49.6	0.0066	1.7727	0.00757	-0.1623
1.05	2862	0.0179	2.153	0.0032	49.5	0.0064	1.7501	0.00764	-0.1564
1.20	2811	0.0165	1.254	0.024	95.3	0.0064	1.6693	0.0676	-0.1407
1.40	2752	0.0148	1.059	0.014	126.8	0.0061	1.6211	0.0583	-0.1234
1.60	2701	0.0133	1.000	0.0006	151.5	0.0059	1.5842	0.0509	-0.1076
1.76	2664	0.0123	1.000	0.0000	165.6	0.0056	1.5426	0.0429	-0.1001
2.00	2615	0.0109	1.011	-0.0008	182.4	0.0054	1.4743	0.0399	-0.0863
4.00	2340	0.0042	1.311	-0.0046	251.2	0.0041	1.2448	0.0159	-0.0366
10.00	1944	-0.0013	2.135	-0.0076	312.2	0.0027	1.0552	0.00030	-0.0044
10.21	1936	-0.0014	2.164	-0.0076	313.2	0.0027	1.0525	0.00049	-0.0040
20.00	1743	-0.0018	3.422	-0.0001	346.1	0.0020	0.9556	0.00066	-0.0018
40.00	1512	-0.0015	5.810	-0.0080	373.2	0.0015	0.9502	0.0001	-0.0005
100.00	1242	-0.0027	10.679	-0.0010	401.3	0.0011	0.894	0.0000	0.0000
200.00	1063	-0.0036	17.764	-0.0018	418.1	0.0005	0.8642	0.0000	0.0000
400.00	904	-0.0038	29.278	-0.0017	431.9	0.0007	0.840	0.0000	0.0000
1000.00	724	-0.0039	55.610	-0.0017	446.5	0.0005	0.8019	0.0000	0.0000
2000.00	606	-0.0040	95.457	-0.0017	455.3	0.0004	0.7643	0.0000	0.0000
4000.00	510	-0.0041	155.133	-0.0017	462.5	0.0003	0.770	0.0000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_e/P	Temperature, $T, ^\circ K$	Temp- erature exponent, n_T	Area ratio, ϵ	Area- ratio exponent, n_ϵ	Specific impulse, $I, (\text{lb/sec})/(\text{lb})$	Specific- impulse exponent, n_I	Specific heat, $c_p, \text{cal}/(\text{lb}^\circ \text{K})$	$(\delta \ln T)/(\delta \ln P)_T$	$(\delta \ln T)/(\delta \ln P)_P$
$R = 0.60, \text{ PERCENT FUEL} = 17.35, \text{ I/F} = 4.762$									
1.00	3097	0.0278							
1.05	3081	0.0273	2.136	0.0028	48.2	0.0097	2.0005	0.01775	-0.3453
1.20	3036	0.0260	1.247	0.0021	92.7	0.0095	2.1752	0.01724	-0.3370
1.40	2985	0.0245	1.055	0.0012	125.3	0.0092	2.0248	0.01435	-0.2887
1.60	2940	0.0232	1.007	0.0005	147.5	0.0090	1.9551	0.01340	-0.2669
1.74	2911	0.0223	1.000	0.0000	159.9	0.0088	1.9107	0.01332	-0.2533
2.00	2865	0.0208	1.013	-0.0008	177.8	0.0086	1.8396	0.01112	-0.2318
4.00	2630	0.0131	1.333	-0.0053	245.9	0.0073	1.5032	0.00605	-0.1359
10.00	2308	0.0028	2.321	-0.0113	307.2	0.0056	1.1598	0.00198	-0.0496
10.21	2300	0.0026	2.352	-0.0115	308.4	0.0055	1.1536	0.00192	-0.0483
20.00	2058	-0.0028	3.708	-0.0146	342.0	0.0044	1.0010	0.00062	-0.0171
40.00	1815	-0.0056	6.038	-0.0159	370.1	0.0034	0.9136	0.00014	-0.0043
100.00	1518	-0.0068	11.693	-0.0161	399.6	0.0124	.8515	0.00001	-0.0004
200.00	1317	-0.0072	19.413	-0.0180	417.4	0.0119	.8157	0.00000	-0.0000
400.00	1135	-0.0075	32.319	-0.0159	432.3	0.0116	.7825	0.00000	-0.0000
1000.00	924	-0.0079	63.444	-0.0159	448.2	0.0112	.7435	0.00000	-0.0000
2000.00	786	-0.0082	105.595	-0.0160	457.9	0.0110	.7189	0.00000	-0.0000
4000.00	665	-0.0084	175.548	-0.0160	466.0	0.0108	.6994	0.00000	-0.0000
$R = 0.70, \text{ PERCENT FUEL} = 15.25, \text{ I/F} = 5.556$									
1.00	3231	0.0365							
1.05	3216	0.0342	2.126	0.0022	46.7	0.0118	2.7036	0.03093	-0.5863
1.20	3176	0.0332	1.242	0.0016	89.8	0.0117	2.6809	0.03031	-0.5771
1.40	3130	0.0320	1.052	0.0010	121.5	0.0115	2.6171	0.02863	-0.5518
1.60	3091	0.0309	1.006	0.0004	143.1	0.0113	2.5409	0.02672	-0.5222
1.74	3068	0.0303	1.000	0.0000	154.2	0.0112	2.4728	0.02509	-0.4963
2.00	3025	0.0291	1.015	-0.0007	172.6	0.0099	2.3550	0.02242	-0.4527
4.00	2823	0.0227	1.348	-0.0044	239.3	0.0099	1.9699	0.01481	-0.3188
10.00	2550	0.0123	2.391	-0.0105	300.2	0.0184	1.4750	0.00697	-0.1640
10.21	2544	0.0121	2.425	-0.0107	301.4	0.0183	1.4650	0.00683	-0.1610
20.00	2331	0.0036	3.886	-0.0180	335.4	0.0171	1.1743	0.00316	-0.0801
40.00	2102	-0.0040	6.425	-0.0207	364.2	0.0159	.9713	0.00111	-0.0305
100.00	1797	-0.0095	12.637	-0.0237	395.0	0.0144	.8358	0.00017	-0.0054
200.00	1579	-0.0110	21.191	-0.0241	413.9	0.0135	.7871	0.00003	-0.0010
400.00	1379	-0.0117	35.638	-0.0241	429.8	0.0129	.7520	0.00000	-0.0001
1000.00	1142	-0.0124	70.952	-0.0242	447.0	0.0122	.7111	0.00000	-0.0000
2000.00	983	-0.0129	119.341	-0.0243	457.6	0.0118	.6825	0.00000	-0.0000
4000.00	841	-0.0134	200.371	-0.0245	466.6	0.0115	.6576	0.00000	-0.0000
$R = 0.80, \text{ PERCENT FUEL} = 13.60, \text{ I/F} = 6.349$									
1.00	3304	0.0387							
1.05	3290	0.0384	2.121	0.0017	45.2	0.0131	3.1245	0.04443	-0.8285
1.20	3253	0.0376	1.240	0.0012	87.0	0.0129	3.1098	0.04384	-0.8209
1.40	3211	0.0367	1.051	0.0007	117.7	0.0126	3.0677	0.04222	-0.7997
1.60	3174	0.0359	1.005	0.0003	136.0	0.0124	3.0156	0.04035	-0.7744
1.74	3154	0.0355	1.000	0.0000	148.9	0.0123	2.9681	0.03872	-0.7517
2.00	3115	0.0345	1.016	-0.0005	167.3	0.0124	2.9401	0.03781	-0.7387
4.00	2935	0.0299	1.357	-0.0032	232.2	0.0116	2.6824	0.03601	-0.7125
10.00	2704	0.0224	2.437	-0.0077	292.0	0.0105	2.0004	0.01710	-0.3892
10.21	2699	0.0222	2.472	-0.0078	293.2	0.0104	2.0482	0.01688	-0.3849
20.00	2526	0.0150	4.017	-0.0123	327.1	0.0093	1.6425	0.01020	-0.2476
40.00	2338	0.0096	6.763	-0.0183	356.3	0.0084	1.2625	0.00500	-0.1301
100.00	2064	-0.0069	13.610	-0.0265	386.1	0.0068	.9242	0.00131	-0.0377
200.00	1840	-0.0126	25.116	-0.0302	408.0	0.0056	.7993	0.00034	-0.0106
400.00	1634	-0.0155	39.267	-0.0315	424.9	0.0046	.7393	0.00006	-0.0042
1000.00	1375	-0.0169	79.186	-0.0318	445.4	0.0036	.6930	0.00000	-0.0002
2000.00	1199	-0.0177	134.669	-0.0300	457.0	0.0030	.6639	0.00000	-0.0000
4000.00	1039	-0.0185	228.324	-0.0322	464.6	0.0025	.6361	0.00000	-0.0000
$R = 0.90, \text{ PERCENT FUEL} = 12.28, \text{ I/F} = 7.143$									
1.00	3336	0.0406							
1.05	3322	0.0404	2.118	0.0015	43.8	0.0136	3.2951	0.05319	-0.9286
1.20	3286	0.0397	1.239	0.0011	84.3	0.0132	3.2773	0.05268	-0.9781
1.40	3246	0.0389	1.021	0.0006	114.0	0.0134	3.2547	0.05127	-0.9625
1.60	3211	0.0383	1.002	0.0002	134.3	0.0132	3.2263	0.04965	-0.9439
1.74	3192	0.0379	1.000	0.0000	146.2	0.0132	3.1957	0.04844	-0.9273
2.00	3154	0.0374	1.016	-0.0004	162.4	0.0132	3.1543	0.04747	-0.9173
4.00	2984	0.0353	1.360	-0.0025	227.4	0.0144	2.9468	0.03662	-0.7946
10.00	2175	0.0266	2.471	-0.0050	261.2	0.0143	2.6506	0.02912	-0.6491
10.21	2170	0.0264	2.493	-0.0057	268.6	0.0142	2.6522	0.02911	-0.6455
20.00	2623	0.0141	4.052	-0.0063	317.9	0.0066	2.3275	0.02207	-0.5207
40.00	2474	0.0183	6.960	-0.0118	346.9	0.0061	1.9360	0.01223	-0.3817
100.00	2267	0.0076	14.362	-0.0140	375.0	0.0040	1.3985	0.00709	-0.1940
200.00	2092	-0.0040	24.776	-0.0171	395.6	0.0030	1.0625	0.00473	-0.0812
400.00	1896	-0.0144	49.107	-0.0344	417.9	0.0028	.6618	0.00073	-0.0424
1000.00	1620	-0.0403	88.419	-0.0161	451.4	0.0024	.6923	0.00000	-0.0029
2000.00	1431	-0.0421	151.900	-0.0357	470.0	0.0021	.6560	0.00001	-0.0004
4000.00	1261	-0.0424	277.745	-0.0370	494.9	0.0016	.6677	0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T , °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_s , lb-sec/lb	Specific-impulse exponent, n_I	Specific heat, c_p , cal/(lb·°K)	$(\frac{\partial \ln M}{\partial \ln P})_T$	$(\frac{\partial \ln M}{\partial \ln T})_P$
$R = 1.00$, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3341	0.0410	2.118	0.0014	42.5	0.0137	3.1852	0.05537	-1.0233
1.05	3328	0.0407	2.118	0.0010	81.8	0.0136	3.1796	0.05488	-1.0184
1.20	3292	0.0401	1.238	0.0006	110.7	0.0134	3.1630	0.05356	-1.0046
1.40	3252	0.0394	1.050	0.0002	130.3	0.0133	3.1421	0.05203	-0.9883
1.60	3217	0.0387	1.005	0.0002	139.8	0.0132	3.1225	0.05071	-0.9736
1.72	3199	0.0384	1.000	0.0000	139.8	0.0132	3.1111	0.04999	-0.9654
2.00	3161	0.0377	1.016	-0.0004	157.3	0.0131	3.0866	0.04851	-0.9483
4.00	2994	0.0344	1.361	-0.0024	218.6	0.0125	2.9493	0.04178	-0.8627
10.00	2789	0.0299	2.462	-0.0051	275.3	0.0117	2.7109	0.03318	-0.7361
10.21	2785	0.0298	2.498	-0.0051	276.4	0.0117	2.7049	0.03300	-0.7331
20.00	2644	0.0264	4.097	-0.0073	308.7	0.0111	2.4914	0.02701	-0.6325
40.00	2505	0.0224	7.007	-0.0097	337.0	0.0105	2.2430	0.02121	-0.5248
100.00	2325	0.0164	14.608	-0.0135	368.5	0.0096	1.8808	0.01429	-0.3815
200.00	2188	0.0108	25.757	-0.0172	389.0	0.0090	1.5942	0.00978	-0.2777
400.00	2048	0.0040	45.624	-0.0218	407.1	0.0082	1.3134	0.00606	-0.1838
1000.00	1850	-0.0070	97.111	-0.0295	427.8	0.0072	0.9862	0.00255	-0.0857
2000.00	1688	-0.0158	170.978	-0.0360	441.5	0.0064	0.8018	0.00103	-0.0380
4000.00	1517	-0.0229	298.702	-0.0412	453.4	0.0055	0.6840	0.00032	-0.0129
$R = 1.50$, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3219	0.0350	2.120	0.0017	37.6	0.0120	1.9992	0.03449	-0.6756
1.05	3206	0.0347	1.240	0.0012	72.4	0.0119	1.9899	0.03400	-0.6690
1.20	3169	0.0340	1.051	0.0007	91.9	0.0117	1.9637	0.03266	-0.6507
1.40	3127	0.0331	1.000	0.0003	115.3	0.0116	1.9320	0.03114	-0.6292
1.60	3091	0.0323	1.005	0.0003	123.9	0.0115	1.9032	0.02983	-0.6103
1.72	3071	0.0318	1.000	0.0000	123.9	0.0113	1.8866	0.02910	-0.5995
2.00	3031	0.0309	1.016	-0.0005	139.2	0.0113	1.8526	0.02767	-0.5780
4.00	2853	0.0265	1.357	-0.0030	192.2	0.0105	1.6765	0.02125	-0.4742
10.00	2626	0.0199	2.439	-0.0069	243.0	0.0095	1.4088	0.01364	-0.3340
10.71	2621	0.0197	2.474	-0.0070	244.0	0.0095	1.4026	0.01348	-0.3309
20.00	2455	0.0140	4.027	-0.0105	272.2	0.0087	1.1931	0.00880	-0.2329
40.00	2281	0.0071	6.005	-0.0149	296.6	0.0078	0.9827	0.00498	-0.1440
100.00	2037	-0.0027	13.824	-0.0214	323.4	0.0065	0.7495	0.00176	-0.0586
200.00	1842	-0.0092	23.661	-0.0258	340.3	0.0055	0.6298	0.00060	-0.0229
400.00	1644	-0.0133	40.695	-0.0284	354.7	0.0046	0.5593	0.00016	-0.0071
1000.00	1393	-0.0458	82.105	-0.0297	370.6	0.0036	0.5103	0.00002	-0.0010
2000.00	1220	-0.167	139.978	-0.0300	380.6	0.0030	0.4869	0.00000	-0.0002
4000.00	1062	-0.175	238.311	-0.0302	389.2	0.0025	0.4666	0.00000	-0.0000
$R = 2.00$, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	3045	0.0278	2.126	0.0020	34.4	0.0100	1.3351	0.01897	-0.4038
1.05	3031	0.0275	1.242	0.0015	66.3	0.0098	1.3254	0.01858	-0.3974
1.20	2992	0.0266	1.052	0.0012	89.7	0.0096	1.2984	0.01750	-0.3799
1.40	2947	0.0255	1.006	0.0009	105.6	0.0094	1.2665	0.01629	-0.3596
1.60	2909	0.0245	1.000	0.0003	113.8	0.0093	1.2381	0.01526	-0.3420
1.72	2886	0.0249	1.000	0.0000	113.8	0.0093	1.2211	0.01467	-0.3316
2.00	2843	0.0229	1.015	-0.0006	127.4	0.0091	1.1894	0.01361	-0.3127
4.00	2649	0.0174	1.348	-0.0038	176.6	0.0082	1.0314	0.00899	-0.2244
10.00	2388	0.0092	2.393	-0.0087	221.6	0.0069	0.8231	0.00434	-0.1226
10.21	2382	0.0091	2.427	-0.0088	224.4	0.0069	0.8187	0.00425	-0.1206
20.00	2184	0.0028	3.895	-0.0128	247.5	0.0059	0.6852	0.00206	-0.0650
40.00	1974	-0.0028	6.456	-0.0164	268.9	0.0049	0.5809	0.00079	-0.0282
100.00	1694	-0.0074	12.751	-0.0192	291.8	0.0037	0.4985	0.00015	-0.0066
200.00	1492	-0.0090	21.403	-0.0199	302.9	0.0030	0.4656	0.00003	-0.0017
400.00	1305	-0.0097	36.042	-0.0200	317.7	0.0024	0.4438	0.00001	-0.0003
1000.00	1084	-0.103	71.914	-0.0200	336.6	0.0019	0.4209	0.00000	-0.0000
2000.00	932	-0.107	121.231	-0.0201	336.7	0.0015	0.4053	0.00000	-0.0000
4000.00	803	-0.111	204.097	-0.0204	345.2	0.0013	0.3906	0.00000	-0.0000
$R = 3.00$, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2695	0.0153	2.145	0.0025	30.3	0.0059	0.7383	0.00555	-0.1399
1.05	2679	0.0149	1.251	0.0018	58.4	0.0057	0.7306	0.00533	-0.1355
1.20	2634	0.0138	1.057	0.0011	78.9	0.0054	0.6854	0.00416	-0.1105
1.40	2582	0.0125	1.007	0.0004	92.8	0.0052	0.6650	0.00368	-0.0997
1.60	2537	0.0114	1.000	0.0000	101.1	0.0051	0.6513	0.00337	-0.0927
1.72	2507	0.0107	1.000	-0.0006	111.9	0.0049	0.6319	0.00295	-0.0830
2.00	2462	0.0096	1.012	-0.0006	134.3	0.0043	0.5411	0.00131	-0.0417
4.00	2220	0.0044	1.320	-0.0038	154.3	0.0038			
10.00	1915	-0.0004	2.211	-0.0057	192.3	0.0027	0.4589	0.00032	-0.0123
10.21	1907	-0.0005	2.301	-0.0067	193.0	0.0026	0.4575	0.00031	-0.0119
20.00	1687	-0.0042	3.601	-0.0076	213.5	0.0020	0.4232	0.00008	-0.0038
40.00	1473	-0.0030	2.851	-0.0074	230.6	0.0015	0.4015	0.00002	-0.0004
100.00	1224	-0.0033	11.252	-0.0071	248.4	0.0011	0.3816	0.00000	-0.0001
200.00	1057	-0.0034	18.558	-0.0076	259.1	0.0009	0.3682	0.00000	-0.0000
400.00	908	-0.0036	30.867	-0.0075	265.1	0.0007	0.3559	0.00000	-0.0000
1000.00	736	-0.0037	60.444	-0.0075	277.6	0.0005	0.3401	0.00000	-0.0000
2000.00	629	-0.0039	100.439	-0.0075	283.4	0.0004	0.3292	0.00000	-0.0000
4000.00	527	-0.0040	165.664	-0.0070	285.2	0.0004	0.3196	0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute.

Pressure ratio, P_c/P	Temperature, $T, {}^\circ K$	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, $I, (lb/sec)/lb$	Specific-impulse exponent, n_I	Specific heat, $c_p, cal/(lb \cdot {}^\circ K)$	$(\frac{\partial \ln I}{\partial \ln P})_T$	$(\frac{\partial \ln I}{\partial \ln T})_P$
R = 4.00, PERCENT FUEL = 3.05, O/F = 1.746									
1.00	2363	0.0064						0.00142	-0.042
1.05	2344	.0061	2.169	0.0018	27.5	0.0026	.4958	.0134	-0.040
1.20	2295	.0053	1.261	0.0013	52.8	.0024	.4833	.0112	-0.034
1.40	2238	.0044	1.062	0.0007	71.3	.0022	.4699	.0091	-0.029
1.60	2188	.0037	1.010	0.0003	83.8	.0021	.4590	.0075	-0.024
1.78	2149	.0032	1.000	0.0000	92.4	.0020	.4509	.0064	-0.021
2.00	2107	.0027	1.009	-0.0003	100.9	.0018	.4426	.0053	-0.018
4.00	1859	.0005	1.295	-0.0016	138.5	.0013	.4044	.0016	-0.006
10.00	1555	-0.0007	2.187	-0.0021	171.5	.0008	.3757	.0002	-0.001
10.21	1549	-0.0007	2.215	-0.0021	172.1	.0008	.3752	.0002	-0.001
20.00	1350	-0.0009	3.431	-0.0021	189.7	.0006	.3616	.0000	-0.002
40.00	1166	-0.0010	5.906	-0.0021	204.2	.0004	.3500	.0000	-0.002
100.00	953	-0.0010	10.485	-0.0020	219.2	.0003	.3353	.0000	-0.000
200.00	814	-0.0011	17.201	-0.0020	228.1	.0004	.3244	.0000	-0.000
400.00	691	-0.0011	28.301	-0.0019	235.5	.0002	.3140	.0000	-0.000
1000.00	552	-0.0011	54.731	-0.0019	243.2	.0001	.3012	.0000	-0.000
2000.00	463	-0.0012	90.095	-0.0020	247.9	.0001	.2928	.0000	-0.000
4000.00	387	-0.0012	148.169	-0.0020	251.7	.0001	.2864	.0000	-0.000
R = 5.00, PERCENT FUEL = 2.45, O/F = 9.683									
1.00	2066	0.0021						0.00033	-0.0118
1.05	2048	.0020	2.188	0.0008	25.2	0.0009	.3996	.0030	-0.0109
1.20	1998	.0016	1.269	.0005	48.4	.0008	.3934	.0024	-0.0089
1.40	1941	.0012	1.066	.0003	65.3	.0007	.3869	.0018	-0.0070
1.60	1892	.0010	1.011	.0001	76.7	.0006	.3818	.0014	-0.0056
1.80	1850	.0007	1.000	0.0000	85.2	.0006	.3777	.0011	-0.0046
2.00	1812	.0006	1.007	-0.0001	92.2	.0005	.3742	.0009	-0.0038
4.00	1578	.0000	1.281	-0.0004	126.2	.0003	.3570	.0002	-0.0010
10.00	1303	-0.0002	2.144	-0.0005	155.7	.0002	.3411	.0000	-0.0001
10.21	1298	-0.0002	2.171	-0.0005	156.3	.0002	.3408	.0000	-0.0001
20.00	1122	-0.0002	3.343	-0.0004	171.9	.0001	.3309	.0000	-0.0000
40.00	961	-0.0003	5.332	-0.0004	184.7	.0001	.3209	.0000	-0.0000
100.00	778	-0.0003	10.068	-0.0004	197.9	.0001	.3076	.0000	-0.0000
200.00	658	-0.0003	16.403	-0.0004	205.6	.0001	.2979	.0000	-0.0000
400.00	554	-0.0003	26.199	-0.0004	214.0	.0000	.2887	.0000	-0.0000
1000.00	438	-0.0003	51.350	-0.0004	218.7	.0000	.2782	.0000	-0.0000
2000.00	365	-0.0003	83.996	-0.0004	222.6	.0000	.2728	.0000	-0.0000
4000.00	303	-0.0003	137.472	-0.0004	225.9	.0000	.2693	.0000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area-ratio exponent, n _ε	Specific impulse, I, lbsec/lb	Specific impulse exponent, n _I	Specific heat, c _p , cal/(lb·°K)	(d ln M) _T (d ln P) _T	(d ln M) _P (d ln T) _P
<i>R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190</i>									
1.00	1183	0.0000						1.7752	0.00000 0.00000
1.05	1168	-0.0000	2.250	0.0000	47.4	0.0000	1.7710	0.00000 0.00000	
1.20	1129	-0.0000	1.297	0.0000	90.8	0.0000	1.7597	0.00000 0.00000	
1.40	1085	-0.0000	1.081	0.0000	122.2	0.0000	1.7472	0.00000 0.00000	
1.60	1049	-0.0000	1.018	0.0000	143.2	0.0000	1.7369	0.00000 0.00000	
1.87	1008	-0.0000	1.000	0.0000	163.4	0.0000	1.7257	0.00000 0.00000	
2.00	989	-0.0000	1.003	0.0000	171.5	0.0000	1.7210	0.00000 0.00000	
4.00	824	-0.0000	1.233	0.0000	232.3	0.0000	1.6825	0.00000 0.00000	
10.00	643	-0.0000	1.974	0.0000	283.1	0.0000	1.6505	0.00000 0.00000	
20.00	532	-0.0000	2.982	0.0000	309.9	0.0000	1.6344	0.00000 0.00000	
20.41	529	-0.0003	3.026	0.0000	310.6	0.0000	1.6339	0.00000 0.00000	
40.00	439	-0.0000	4.520	0.0000	333.4	0.0000	1.6267	0.00000 0.00000	
100.00	340	-0.0000	8.432	0.0000	390.8	0.0000	1.6099	0.00000 0.00000	
200.00	280	-0.0000	12.431	0.0000	362.6	0.0000	1.5970	0.00000 0.00000	
400.00	230	-0.0000	21.488	0.0000	372.0	0.0000	1.5571	0.00000 0.00000	
1000.00	175	-0.0000	39.928	0.0000	381.6	0.0000	1.4840	0.00000 0.00000	
2000.00	142	-0.0000	63.572	0.0000	387.2	0.0000	1.4287	0.00000 0.00000	
4000.00	114	-0.0000	100.938	0.0000	391.6	0.0000	1.4046	0.00000 0.00000	
<i>R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587</i>									
1.00	1514	0.0000						1.6188	0.00000 0.00000
1.05	1497	-0.002	2.233	0.0000	49.3	0.0000	1.6144	0.00000 0.00000	
1.20	1450	-0.0000	1.289	0.0000	94.6	0.0000	1.6025	0.00000 0.00000	
1.40	1398	-0.0000	1.077	0.0000	121.4	0.0000	1.5889	0.00000 0.00000	
1.60	1354	-0.0000	1.016	0.0000	149.4	0.0000	1.5773	0.00000 0.00000	
1.87	1307	-0.0000	1.000	0.0000	169.2	0.0000	1.5652	0.00000 0.00000	
2.00	1282	-0.0000	1.004	0.0000	179.1	0.0000	1.5585	0.00000 0.00000	
4.00	1079	-0.0000	1.244	0.0000	242.2	0.0000	1.5046	0.00000 0.00000	
10.00	852	-0.0000	2.009	0.0000	297.2	0.0000	1.4516	0.00000 0.00000	
20.00	709	-0.0000	3.049	0.0000	325.9	0.0000	1.4232	0.00000 0.00000	
20.41	705	-0.0000	3.088	0.0000	326.7	0.0000	1.4225	0.00000 0.00000	
40.00	588	-0.0000	4.739	0.0000	348.0	0.0000	1.4065	0.00000 0.00000	
100.00	458	-0.0000	6.679	0.0000	370.0	0.0000	1.3913	0.00000 0.00000	
200.00	379	-0.0000	12.870	0.0000	362.7	0.0000	1.3807	0.00000 0.00000	
400.00	312	-0.0000	24.296	0.0000	393.0	0.0000	1.3677	0.00000 0.00000	
1000.00	242	-0.0000	41.979	0.0000	403.5	0.0000	1.3402	0.00000 0.00000	
2000.00	198	-0.0000	67.687	0.0000	409.7	0.0000	1.2977	0.00000 0.00000	
4000.00	161	-0.0000	108.755	0.0000	414.6	0.0000	1.2571	0.00000 0.00000	
<i>R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984</i>									
1.00	1817	0.0001						1.5015	0.00002 -0.0006
1.05	1797	-0.0001	2.218	0.0001	50.3	0.0001	1.4971	0.00002 -0.0005	
1.20	1742	-0.0001	1.283	0.0000	96.6	0.0000	1.4852	0.00001 -0.0004	
1.40	1686	-0.0000	1.073	0.0000	130.1	0.0000	1.4719	0.00001 -0.0002	
1.60	1635	-0.0000	1.015	0.0000	152.7	0.0000	1.4609	0.00000 -0.0002	
1.87	1587	-0.0000	1.000	0.0000	171.8	0.0000	1.4499	0.00000 -0.0001	
2.00	1555	-0.0000	1.005	0.0000	183.1	0.0000	1.4425	0.00000 -0.0001	
4.00	1322	-0.0000	1.256	0.0000	249.3	0.0000	1.3875	0.00000 -0.0000	
10.00	1057	-0.0000	2.048	0.0000	305.6	0.0000	1.3226	0.00000 0.00000	
20.00	887	-0.0000	3.127	0.0000	335.7	0.0000	1.2849	0.00000 0.00000	
20.41	882	-0.0000	3.168	0.0000	336.5	0.0000	1.2838	0.00000 0.00000	
40.00	741	-0.0000	4.883	0.0000	359.0	0.0000	1.2560	0.00000 0.00000	
100.00	541	-0.0000	6.485	0.0000	382.4	0.0000	1.2421	0.00000 0.00000	
200.00	482	-0.0000	14.396	0.0000	395.9	0.0000	1.2192	0.00000 0.00000	
400.00	399	-0.0003	23.208	0.0000	406.8	0.0000	1.2099	0.00000 0.00000	
1000.00	310	-0.0000	43.854	0.0000	416.1	0.0000	1.1949	0.00000 0.00000	
2000.00	256	-0.0000	71.280	0.0000	424.7	0.0000	1.1801	0.00000 0.00000	
4000.00	210	-0.0000	115.650	0.0000	430.2	0.0000	1.1475	0.00000 0.00000	
<i>R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381</i>									
1.00	2093	0.0008						1.4230	0.00014 -0.0038
1.05	2072	-0.0007	2.206	0.0000	50.8	0.0000	1.4174	0.00013 -0.0035	
1.20	2016	-0.0005	1.277	0.0002	97.5	0.0003	1.4027	0.00010 -0.0026	
1.40	1952	-0.0004	1.970	0.0001	131.4	0.0002	1.3869	0.00007 -0.0019	
1.60	1897	-0.0004	1.013	0.0000	154.2	0.0002	1.3740	0.00005 -0.0014	
1.87	1846	-0.0004	1.000	0.0000	172.7	0.0002	1.3623	0.00003 -0.0010	
2.00	1809	-0.0001	1.006	0.0000	185.1	0.0002	1.3539	0.00003 -0.0008	
4.00	1553	-0.0000	1.266	-0.0001	252.6	0.0001	1.2994	0.00000 -0.0001	
10.00	1257	-0.0001	2.085	-0.0001	310.4	0.0000	1.2336	0.00000 0.00000	
20.00	1064	-0.0001	3.206	-0.0001	341.7	0.0000	1.1891	0.00000 0.00000	
20.41	1059	-0.0001	3.248	-0.0001	342.5	0.0000	1.1878	0.00000 0.00000	
40.00	895	-0.0001	5.037	-0.0001	366.0	0.0000	1.1531	0.00000 0.00007	
1000.00	707	-0.0001	9.325	-0.0001	390.5	0.0000	1.1173	0.00000 0.00000	
2000.00	590	-0.0001	14.993	-0.0000	404.8	0.0000	1.1006	0.00000 0.00000	
4000.00	493	-0.0001	24.234	-0.0000	416.3	0.0000	1.0855	0.00000 0.00000	
1000.00	383	-0.0001	46.000	-0.0000	428.3	0.0000	1.0745	0.00000 0.00000	
2000.00	317	-0.0001	74.914	-0.0000	455.4	0.0000	1.0637	0.00000 0.00000	
4000.00	262	-0.0001	124.189	-0.0001	474.2	0.0000	1.0223	0.00000 0.00000	

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T_c , °K	Temperature exponent, n_t	Area ratio, ϵ	Aero-ratio exponent, n_E	Specific impulse, I_s , (lb/sec)/lb	Specific impulse exponent, n_I	Specific heat, c_p , cal/(g·°K)	$(\partial \ln \mathfrak{R})_T / (\partial \ln P)_T$	$(\partial \ln \mathfrak{R})_P / (\partial \ln T)_P$
$R = 0.35$, PERCENT FUEL = 26.41, O/F = 2.778									
1.00	2344	0.0026						1.3936	0.00059
1.05	2322	0.0024	1.194	0.0004	50.9	0.0010	1.3850	0.00054	-0.0141
1.20	2263	0.0019	1.272	0.0006	97.7	0.0009	1.3629	0.00042	-0.0104
1.40	2198	0.0014	1.068	0.0004	131.7	0.0008	1.3398	0.00031	-0.0079
1.60	2139	0.0011	1.012	0.0001	154.7	0.0007	1.3219	0.00024	-0.0062
1.80	2088	0.0008	1.000	0.0000	172.3	0.0006	1.3072	0.00018	-0.0049
2.00	2045	0.0006	1.007	-0.0001	185.8	0.0006	1.2955	0.00015	-0.0040
4.00	1771	-0.0001	1.275	-0.0004	254.0	0.0014	1.2510	0.00003	-0.0008
10.00	1451	-0.0003	2.119	-0.0004	313.0	0.0014	1.1857	0.00000	+0.0000
20.00	1238	-0.0003	3.281	-0.0004	345.1	0.001	1.1205	0.00000	+0.0000
20.41	1232	-0.0003	3.325	-0.0004	345.9	0.001	1.1192	0.00000	+0.0000
40.00	1051	-0.0003	5.189	-0.0004	372.2	0.001	1.0794	0.00000	+0.0000
100.00	838	-0.0003	9.678	-0.0004	395.8	0.001	1.0365	0.00000	+0.0000
200.00	702	-0.0003	15.630	-0.0003	410.8	0.001	1.0119	0.00000	+0.0000
400.00	586	-0.0003	25.355	-0.0003	422.9	0.0010	0.9954	0.00000	+0.0000
1000.00	460	-0.0003	48.298	-0.0003	435.5	0.0010	0.9791	0.00000	+0.0000
2000.00	382	-0.0003	78.866	-0.0003	443.0	0.0000	0.9692	0.00000	+0.0000
4000.00	317	-0.0003	128.975	-0.0003	449.2	0.0000	0.9598	0.00000	+0.0000
$R = 0.40$, PERCENT FUEL = 23.95, O/F = 3.175									
1.00	2565	0.0061						1.4467	0.00163
1.05	2543	0.0057	2.181	0.0018	20.7	0.0005	1.4084	0.00152	-0.0341
1.20	2484	0.0048	1.267	0.0013	97.4	0.001	1.3764	0.00125	-0.0286
1.40	2417	0.0038	1.065	0.0007	131.4	0.0009	1.3423	0.00098	-0.0230
1.60	2359	0.0031	1.011	0.0003	154.4	0.0007	1.3153	0.00079	-0.0188
1.79	2310	0.0025	1.000	0.0000	171.1	0.0006	1.2941	0.00065	-0.0158
2.00	2263	0.0020	1.008	-0.0003	185.6	0.005	1.2752	0.00053	-0.0137
4.00	1978	0.0001	1.285	-0.0013	254.2	0.0009	1.1857	0.00013	-0.0036
10.00	1637	-0.0006	2.152	-0.0015	314.0	0.0016	1.1119	0.00001	-0.0004
20.00	1409	-0.0007	3.354	-0.0014	346.8	0.004	1.0671	0.00000	+0.0000
20.41	1403	-0.0007	3.399	-0.0014	347.6	0.004	1.0658	0.00000	+0.0000
40.00	1205	-0.0008	5.338	-0.0014	372.6	0.003	1.0255	0.00000	+0.0000
100.00	970	-0.0008	10.036	-0.0013	399.1	0.0014	0.9768	0.00000	+0.0000
200.00	819	-0.0008	16.294	-0.0013	414.7	0.002	0.9478	0.00000	+0.0000
400.00	687	-0.0008	26.545	-0.0013	427.4	0.001	0.9290	0.00000	+0.0000
1000.00	542	-0.0009	50.799	-0.0013	440.7	0.001	0.9038	0.00000	+0.0000
2000.00	452	-0.0009	83.167	-0.0013	448.6	0.001	0.8829	0.00000	+0.0000
4000.00	376	-0.0009	136.362	-0.0013	455.1	0.001	0.8831	0.00000	+0.0000
$R = 0.45$, PERCENT FUEL = 21.67, O/F = 3.571									
1.00	2755	0.0107						1.5003	0.00351
1.05	2734	0.0102	2.169	0.0026	50.3	0.0009	1.4843	0.00332	-0.0704
1.20	2677	0.0090	1.261	0.0019	96.7	0.007	1.4419	0.00283	-0.0610
1.40	2611	0.0076	1.062	0.0011	136.4	0.004	1.3959	0.00233	-0.0513
1.60	2555	0.0065	1.010	0.0005	153.4	0.002	1.3588	0.00195	-0.0438
1.78	2510	0.0056	1.000	0.0000	169.1	0.000	1.3312	0.00168	-0.0384
2.00	2460	0.0048	1.009	-0.0003	184.6	0.008	1.3023	0.00142	-0.0329
4.00	2173	0.0010	1.295	-0.0026	252.4	0.000	1.1697	0.00044	-0.0113
10.00	1818	-0.0010	2.187	-0.0015	313.8	0.0014	1.1117	0.00006	-0.0017
20.00	1576	-0.0014	3.427	-0.0014	347.2	0.019	1.0246	0.00001	-0.0003
20.41	1569	-0.0014	3.474	-0.0014	348.1	0.019	1.0233	0.00001	-0.0003
40.00	1358	-0.0015	5.487	-0.0013	373.6	0.016	0.9831	0.00000	+0.0000
100.00	1105	-0.0016	10.401	-0.0012	400.9	0.015	0.9327	0.00000	+0.0000
200.00	938	-0.0017	16.983	-0.0012	417.1	0.014	0.8999	0.00000	+0.0000
400.00	793	-0.0017	27.808	-0.0012	430.4	0.013	0.8728	0.00000	+0.0000
1000.00	630	-0.0018	53.499	-0.0012	444.3	0.014	0.8465	0.00000	+0.0000
2000.00	527	-0.0018	87.879	-0.0012	452.6	0.014	0.8315	0.00000	+0.0000
4000.00	440	-0.0018	144.466	-0.0012	459.5	0.014	0.8211	0.00000	+0.0000
$R = 0.50$, PERCENT FUEL = 20.12, O/F = 3.968									
1.00	2915	0.0158						1.6231	0.00633
1.05	2895	0.0153	2.158	0.0029	49.8	0.0016	1.6042	0.00604	-0.1225
1.20	2841	0.0139	1.256	0.0022	95.7	0.0014	1.5535	0.00531	-0.1095
1.40	2778	0.0123	1.060	0.0013	129.4	0.001	1.4970	0.00454	-0.0953
1.60	2724	0.0109	1.007	0.0006	152.0	0.0019	1.4502	0.00393	-0.0838
1.77	2684	0.0099	1.000	0.0000	166.6	0.0017	1.4166	0.00351	-0.0760
2.00	2633	0.0087	1.010	-0.0007	183.0	0.0014	1.3768	0.00303	-0.0667
4.00	2352	0.0030	1.507	-0.0039	251.9	0.0013	1.1932	0.00116	-0.0281
10.00	1992	-0.0012	2.224	-0.0011	312.7	0.0014	1.0508	0.00021	-0.0059
20.00	1740	-0.0023	3.504	-0.0014	346.6	0.0116	0.9116	0.00004	-0.0012
20.41	1732	-0.0023	3.553	-0.0014	347.2	0.0116	0.9004	0.00004	-0.0012
40.00	1509	-0.0026	5.642	-0.0013	373.5	0.0114	0.8491	0.00001	-0.0004
100.00	1240	-0.0028	10.777	-0.0011	401.5	0.0118	0.8988	0.00000	+0.0000
200.00	1060	-0.0029	17.699	-0.0011	416.5	0.0117	0.8638	0.00000	+0.0000
400.00	902	-0.0030	29.139	-0.0010	432.1	0.0117	0.8336	0.00000	+0.0000
1000.00	722	-0.0011	56.410	-0.0010	446.6	0.0114	0.8015	0.00000	+0.0000
2000.00	607	-0.0012	93.015	-0.0010	455.4	0.0114	0.7842	0.00000	+0.0000
4000.00	506	-0.0013	153.404	-0.0010	464.7	0.0114	0.7698	0.00000	+0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, $T, ^\circ K$	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, $I, (lb-sec)/lb$	Specific-impulse exponent, n_I	Specific heat, $c_p, cal/(lb \cdot ^\circ K)$	$(\partial \ln \frac{m}{P})_T$	$(\partial \ln \frac{m}{P})_P$
$R = 0.60, \text{ PERCENT FUEL} = 17.35, \text{ O/F} = 4.762$									
1.00	3155	0.0254	2.140	0.0028	48.5	0.0088	1.9667	0.01480	-0.2833
1.05	3137	0.0249	1.248	0.0021	93.3	0.0085	1.9446	0.01434	-0.2759
1.20	3089	0.0235	1.056	0.0013	126.1	0.0083	1.8842	0.01312	-0.2559
1.40	3033	0.0220	1.007	0.0005	148.6	0.0080	1.8145	0.01177	-0.2335
1.60	2985	0.0206	1.000	0.0000	161.2	0.0079	1.7545	0.01067	-0.2145
1.75	2953	0.0197	1.013	-0.0008	178.8	0.0076	1.7154	0.0097	-0.2024
2.00	2904	0.0182	1.328	-0.0051	247.0	0.0064	1.6559	0.00894	-0.1843
4.00	2652	0.0106	5.977	-0.0136	370.9	0.0028	1.3741	0.00466	-0.1037
10.00	2311	0.0015	2.303	-0.0104	308.3	0.0047	1.0984	0.00142	-0.0356
20.00	2054	-0.0029	3.673	-0.0127	343.0	0.0035	0.9752	0.00043	-0.0118
20.41	2047	-0.0029	3.726	-0.0128	343.9	0.0036	0.9726	0.00041	-0.0113
40.00	1808	-0.0049	5.977	-0.0136	370.9	0.0028	0.9053	0.00009	-0.0049
100.00	1512	-0.0058	11.573	-0.0136	400.2	0.0020	0.8496	0.00001	-0.0003
200.00	1311	-0.0061	19.216	-0.0135	418.0	0.0016	0.8145	0.00000	-0.0007
400.00	1130	-0.0063	31.993	-0.0134	432.0	0.0013	0.7815	0.00000	-0.0000
1000.00	919	-0.0066	62.803	-0.0134	448.6	0.0010	0.7427	0.00000	-0.0000
2000.00	782	-0.0069	104.524	-0.0135	458.2	0.0008	0.7183	0.00000	-0.0000
4000.00	661	-0.0071	173.763	-0.0135	466.3	0.0007	0.6988	0.00000	-0.0000
$R = 0.70, \text{ PERCENT FUEL} = 15.25, \text{ O/F} = 5.556$									
1.00	3307	0.0328	2.129	0.0023	47.0	0.0111	2.3992	0.02681	-0.4983
1.05	3291	0.0324	1.294	0.0017	90.6	0.0109	2.3785	0.02623	-0.4898
1.20	3248	0.0314	1.053	0.0010	122.4	0.0107	2.3205	0.02465	-0.4663
1.40	3198	0.0301	1.006	0.0004	144.1	0.0105	2.2512	0.02286	-0.4389
1.60	3156	0.0289	1.000	0.0000	155.6	0.0104	2.1898	0.02134	-0.4151
1.73	3130	0.0282	1.014	-0.0007	173.9	0.0104	2.1520	0.02044	-0.4007
2.00	3085	0.0269	1.344	-0.0046	240.8	0.0091	2.0841	0.01889	-0.3752
4.00	2865	0.0201	5.977	-0.0136	361.6	0.0051	1.7441	0.01201	-0.2554
10.00	2569	0.0096	2.374	-0.0108	301.9	0.0075	1.3258	0.00529	-0.1237
20.00	2335	0.0015	3.843	-0.0156	336.9	0.0063	1.0849	0.00226	-0.0572
20.41	2328	0.0013	3.900	-0.0158	337.9	0.0062	1.0791	0.00219	-0.0557
40.00	2095	-0.0047	6.337	-0.0193	361.6	0.0051	0.9294	0.00075	-0.0206
100.00	1785	-0.0086	12.441	-0.0212	396.1	0.0038	0.8253	0.00011	-0.0035
200.00	1568	-0.0097	20.858	-0.0214	414.9	0.0030	0.7835	0.00002	-0.0006
400.00	1368	-0.0102	35.080	-0.0214	430.6	0.0025	0.7500	0.00000	-0.0001
1000.00	1133	-0.0108	69.841	-0.0214	447.6	0.0019	0.7094	0.00000	-0.0000
2000.00	975	-0.0113	117.461	-0.0215	458.2	0.0016	0.6811	0.00000	-0.0000
4000.00	834	-0.0117	197.192	-0.0217	467.0	0.0013	0.6564	0.00000	-0.0000
$R = 0.80, \text{ PERCENT FUEL} = 13.60, \text{ O/F} = 6.349$									
1.00	3393	0.0377	2.123	0.0018	45.6	0.0126	2.7921	0.03990	-0.7279
1.05	3378	0.0374	1.241	0.0013	87.8	0.0124	2.7781	0.03933	-0.7206
1.20	3338	0.0366	1.052	0.0008	118.7	0.0122	2.7382	0.03775	-0.7001
1.40	3292	0.0356	1.000	0.0003	139.8	0.0121	2.6891	0.03593	-0.6756
1.60	3253	0.0347	1.005	-0.0002	150.4	0.0120	2.6439	0.03435	-0.6538
1.73	3231	0.0342	1.016	-0.0004	163.7	0.0118	2.6168	0.03365	-0.6410
2.00	3189	0.0332	1.354	-0.0005	234.0	0.0110	2.5628	0.03173	-0.6167
4.00	2995	0.0282	5.977	-0.0134	394.0	0.0010	2.2689	0.02369	-0.4897
10.00	2744	0.0199	2.423	-0.0083	294.1	0.0098	1.8019	0.01386	-0.3122
20.00	2550	0.0118	3.982	-0.0132	329.1	0.0088	1.4368	0.00226	-0.1878
20.41	2544	0.0116	4.042	-0.0134	330.1	0.0087	1.4265	0.00763	-0.1844
40.00	2344	0.0025	6.676	-0.0191	358.3	0.0076	1.1265	0.00355	-0.0722
100.00	2053	-0.0080	13.365	-0.0258	389.8	0.0060	0.8717	0.00085	-0.0245
200.00	1830	-0.0123	22.652	-0.0282	409.5	0.0050	0.7805	0.00021	-0.0066
400.00	1617	-0.0141	38.453	-0.0289	426.2	0.0041	0.7331	0.00004	-0.0013
1000.00	1360	-0.0152	77.533	-0.0291	444.6	0.0031	0.6903	0.00000	-0.0001
2000.00	1185	-0.0159	131.747	-0.0292	455.9	0.0026	0.6615	0.00000	-0.0000
4000.00	1027	-0.0166	223.495	-0.0294	465.6	0.0022	0.6339	0.00000	-0.0000
$R = 0.90, \text{ PERCENT FUEL} = 12.28, \text{ O/F} = 7.143$									
1.00	3430	0.0401	2.121	0.0015	44.2	0.0132	2.9626	0.04890	-0.8833
1.05	3416	0.0399	1.240	0.0011	85.1	0.0131	2.9553	0.04840	-0.8780
1.20	3377	0.0391	1.051	0.0006	115.1	0.0129	2.9343	0.04704	-0.8631
1.40	3334	0.0383	1.005	-0.0002	135.5	0.0128	2.9078	0.04546	-0.8452
1.60	3296	0.0376	1.000	-0.0004	145.5	0.0127	2.8830	0.04409	-0.8291
1.73	3276	0.0372	1.000	-0.0004	163.5	0.0126	2.8682	0.04332	-0.8199
2.00	3235	0.0364	1.016	-0.0004	163.5	0.0126	2.8374	0.04180	-0.8012
4.00	3054	0.0326	1.358	-0.0026	227.1	0.0119	2.6636	0.03473	-0.7059
10.00	2829	0.0271	2.448	-0.0058	285.6	0.0110	2.3536	0.02551	-0.5605
20.00	2666	0.0222	4.058	-0.0088	320.2	0.0103	2.0547	0.01871	-0.4366
20.41	2661	0.0220	4.121	-0.0089	321.2	0.0103	2.0450	0.01851	-0.4328
40.00	2503	0.0158	6.901	-0.0128	349.2	0.0095	1.7023	0.01221	-0.3040
100.00	2276	0.0037	14.187	-0.0208	381.3	0.0083	1.2030	0.00498	-0.1364
200.00	2084	-0.0074	24.518	-0.0284	401.7	0.0073	0.9125	0.00171	-0.0508
400.00	1877	-0.0152	42.200	-0.0336	419.4	0.0061	0.7617	0.00042	-0.0136
1000.00	1606	-0.0192	66.184	-0.0357	439.0	0.0048	0.6840	0.00004	-0.0016
2000.00	1416	-0.0204	147.806	-0.0361	451.3	0.0040	0.6520	0.00001	-0.0002
4000.00	1241	-0.0213	253.224	-0.0363	462.0	0.0034	0.6246	0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T_c , °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_{sp} , lb/sec/lb	Specific-impulse exponent, n_I	Specific heat, c_p , cal/(lb·°K)	$(\frac{\partial \ln M}{\partial \ln P})_T$	$(\frac{\partial \ln M}{\partial \ln T})_P$
$R = 1.00$, PERCENT FUEL = 11.19, O/F = 1.937									
1.00	3437	0.0405	2.120	0.0014	42.9	0.013	2.8811	0.05123	-0.9244
1.05	3423	0.0403	2.120	0.0010	82.6	0.012	2.8760	0.05076	-0.9197
1.20	3384	0.0396	1.239	0.0010	111.7	0.011	2.8611	0.04948	-0.9067
1.40	3341	0.0389	1.051	0.0006	131.5	0.010	2.8421	0.04800	-0.8912
1.60	3304	0.0382	1.005	0.0002	141.3	0.010	2.8243	0.04672	-0.8773
1.72	3284	0.0378	1.000	0.0000	141.3	0.010	2.8138	0.04601	-0.8693
2.00	3244	0.0371	1.016	0.0004	158.0	0.017	2.7914	0.04460	-0.8532
4.00	3065	0.0356	1.359	0.0024	240.4	0.011	2.6657	0.03811	-0.7719
10.00	2847	0.0289	2.493	0.0052	277.7	0.013	2.4459	0.02986	-0.6519
20.00	2692	0.0251	4.076	0.0075	311.1	0.017	2.2431	0.02398	-0.5541
20.41	2687	0.0250	4.140	0.0075	312.0	0.016	2.2367	0.02381	-0.5512
40.00	2542	0.0209	6.959	0.0100	339.4	0.010	2.0143	0.01851	-0.4532
100.00	2349	0.0144	14.469	0.0141	370.9	0.004	1.6831	0.01209	-0.3207
200.00	2203	0.0084	25.445	0.0180	391.3	0.005	1.4246	0.00801	-0.2268
400.00	2052	0.0014	44.925	0.0228	409.3	0.007	1.1770	0.00475	-0.1443
1000.00	1839	-0.0094	95.113	-0.0303	429.9	0.007	0.8997	0.00185	-0.0626
2000.00	1668	-0.0171	166.760	-0.0360	449.3	0.008	0.7520	0.00070	-0.0260
4000.00	1493	-0.0227	290.406	-0.0400	455.0	0.0050	0.6606	0.00020	-0.0083
$R = 1.50$, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3297	0.0338	2.123	0.0017	37.9	0.013	1.8003	0.03075	-0.5921
1.05	3282	0.0335	2.123	0.0012	75.0	0.014	1.7419	0.03029	-0.5859
1.20	3243	0.027	1.241	0.0012	98.7	0.012	1.7680	0.02902	-0.5689
1.40	3198	0.018	1.02	0.0007	98.7	0.012	1.7591	0.02758	-0.5480
1.60	3159	0.009	1.005	0.0003	118.2	0.010	1.7131	0.02635	-0.5312
1.73	3137	0.004	1.000	0.0000	125.0	0.010	1.6977	0.02565	-0.5210
2.00	3096	0.0295	1.015	0.0005	140.2	0.018	1.6672	0.02432	-0.5012
4.00	2904	0.0249	1.354	0.0031	194.6	0.010	1.5078	0.01834	-0.4053
10.00	2661	0.0179	2.427	0.0071	244.6	0.009	1.2577	0.01140	-0.2780
20.00	2478	0.0118	3.997	0.0108	273.8	0.001	1.0774	0.00711	-0.1886
20.41	2472	0.0116	4.058	0.0110	274.6	0.000	1.0719	0.00700	-0.1862
40.00	2291	0.0050	6.734	0.0151	298.2	0.001	0.8963	0.00387	-0.1128
100.00	2032	-0.0040	13.621	-0.0211	324.8	0.009	0.7030	0.00129	-0.0437
200.00	1830	-0.0093	23.271	-0.0445	341.5	0.009	0.6070	0.00043	-0.0167
400.00	1629	-0.0125	39.732	-0.0664	355.8	0.001	0.5000	0.00011	-0.0051
1000.00	1379	-0.0144	80.499	-0.0273	371.5	0.002	0.5072	0.00001	-0.0007
2000.00	1207	-0.0152	137.214	-0.0276	381.4	0.007	0.4850	0.00000	-0.0001
4000.00	1050	-0.0159	233.567	-0.0278	389.8	0.004	0.4650	0.00000	-0.0000
$R = 2.00$, PERCENT FUEL = 5.92, O/F = 1.873									
1.00	3103	0.0252	2.129	0.0020	34.7	0.003	1.2138	0.01648	-0.3472
1.05	3088	0.0258	2.129	0.0015	66.7	0.002	1.2052	0.01611	-0.3414
1.20	3046	0.0249	2.123	0.0015	66.7	0.002	1.1812	0.01513	-0.3259
1.40	2998	0.0237	1.053	0.0009	90.2	0.000	1.1528	0.01402	-0.3074
1.60	2957	0.0228	1.006	0.0003	105.2	0.008	1.1276	0.01309	-0.2914
1.73	2932	0.0222	1.000	0.0000	114.7	0.007	1.1122	0.01255	-0.2819
2.00	2889	0.0211	1.014	-0.0006	128.2	0.005	1.0844	0.01160	-0.2651
4.00	2679	0.0155	1.344	-0.0038	177.5	0.005	0.9449	0.00749	-0.1868
10.00	2402	0.0076	2.379	-0.0086	222.6	0.003	0.7644	0.00348	-0.0990
20.00	2188	0.0017	3.861	-0.0123	248.5	0.003	0.6477	0.00160	-0.0512
20.41	2181	0.0015	3.918	-0.0124	249.2	0.002	0.6447	0.00156	-0.0501
40.00	1970	-0.0031	6.385	-0.0153	265.8	0.003	0.5611	0.00060	-0.0218
100.00	1686	-0.0068	12.580	-0.0174	292.5	0.003	0.4923	0.00012	-0.0051
200.00	1483	-0.0080	21.125	-0.0179	305.5	0.006	0.4632	0.00003	-0.0013
400.00	1297	-0.0086	35.572	-0.0160	318.2	0.001	0.4427	0.00000	-0.0004
1000.00	1076	-0.0092	70.973	-0.0180	331.0	0.006	0.4201	0.00000	-0.0000
2000.00	929	-0.0095	119.641	-0.0180	338.9	0.004	0.4046	0.00000	-0.0000
4000.00	797	-0.0099	201.392	-0.0182	345.0	0.001	0.3900	0.00000	-0.0000
$R = 3.00$, PERCENT FUEL = 4.03, O/F = 1.810									
1.00	2723	0.0136	2.148	0.0023	30.5	0.004	0.6969	0.00463	-0.1169
1.05	2705	0.0132	2.148	0.0017	58.6	0.000	0.6842	0.00445	-0.1131
1.20	2658	0.0122	1.252	0.0017	94.0	0.000	0.6659	0.00396	-0.1029
1.40	2604	0.0110	1.058	0.0010	75.2	0.008	0.6451	0.00344	-0.0917
1.60	2556	0.0100	1.008	0.0004	93.1	0.006	0.6275	0.00303	-0.0825
1.73	2523	0.0093	1.000	0.0000	101.6	0.005	0.6155	0.00276	-0.0763
2.00	2477	0.0083	1.012	-0.0008	112.2	0.003	0.5991	0.00241	-0.0682
4.00	2232	0.0036	1.317	-0.0034	154.7	0.003	0.5216	0.00106	-0.0398
10.00	1914	-0.0005	2.261	-0.0058	192.6	0.003	0.4517	0.00026	-0.0094
20.00	1684	-0.0020	3.584	-0.0065	213.8	0.007	0.4206	0.00007	-0.0030
20.41	1678	-0.0020	3.634	-0.0065	214.4	0.007	0.4199	0.00006	-0.0024
40.00	1472	-0.0026	5.802	-0.0066	230.8	0.003	0.4007	0.00001	-0.0007
100.00	1222	-0.0028	11.177	-0.0065	248.6	0.009	0.3813	0.00000	-0.0001
200.00	1055	-0.0030	18.498	-0.0065	259.3	0.007	0.3680	0.00000	-0.0000
400.00	906	-0.0031	30.718	-0.0054	268.2	0.006	0.3557	0.00000	-0.0000
1000.00	735	-0.0032	60.124	-0.0054	277.7	0.005	0.3399	0.00000	-0.0000
2000.00	623	-0.0033	98.958	-0.0064	283.5	0.004	0.3291	0.00000	-0.0000
4000.00	526	-0.0034	165.857	-0.0065	288.3	0.003	0.3195	0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIO RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T_c , K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_s , lb-sec/lb	Specific-impulse exponent, n_I	Specific heat, c_p , cal/(g°C_K)	$(\frac{\partial \ln I_s}{\partial \ln P})_T$	$(\frac{\partial \ln I_s}{\partial \ln T})_P$
$R = 4.00, \text{ PERCENT FULL} = 3.05, \text{ O/F} = 1.746$									
1.00	2372	0.0055					0.4836	0.00116	-0.0351
1.05	2354	0.0052	2.172	0.0015	27.5	0.0022	4.796	.00104	-0.0333
1.20	2303	0.0045	1.262	0.0011	52.9	0.0021	4.689	.00091	-0.0287
1.40	2244	0.0037	1.063	0.0006	71.4	0.0019	4.574	.00074	-0.0239
1.60	2194	0.0031	1.010	0.0003	83.9	0.0018	4.481	.00061	-0.0203
1.78	2153	0.0027	1.000	0.0000	92.6	0.0017	4.412	.0002	-0.0177
2.00	2110	0.0022	1.009	-0.0003	101.0	0.0016	4.341	.00043	-0.0151
4.00	1859	0.0004	1.294	-0.0013	138.6	0.0011	4.010	.00013	-0.0053
10.00	1555	-0.0006	4.184	-0.0018	171.6	0.0006	3.749	.00002	-0.0009
20.00	1349	-0.0007	3.426	-0.0018	189.8	0.0005	3.614	.00000	-0.0002
20.41	1343	-0.0008	3.475	-0.0018	196.2	0.0005	3.611	.00000	-0.0004
40.00	1165	-0.0008	5.499	-0.0017	204.2	0.0003	3.499	.00000	-0.0000
100.00	952	-0.0009	10.472	-0.0016	219.4	0.0002	3.352	.00000	-0.0000
200.00	813	-0.0009	17.179	-0.0016	228.1	0.0002	3.243	.00000	-0.0000
400.00	690	-0.0009	28.266	-0.0016	235.5	0.0002	3.139	.00000	-0.0000
1000.00	552	-0.0009	54.663	-0.0016	243.2	0.0001	3.012	.00000	-0.0000
2000.00	463	-0.0010	89.984	-0.0016	247.9	0.0001	2.928	.00000	-0.0000
4000.00	386	-0.0010	147.985	-0.0016	251.8	0.0001	2.864	.00000	-0.0000
$R = 5.00, \text{ PERCENT FUEL} = 2.45, \text{ O/F} = 9.683$									
1.00	2069	0.0018					0.3966	0.00027	-0.0097
1.05	2051	.0016	2.189	0.0006	25.2	0.0007	3.947	.00025	-0.0090
1.20	2000	0.0013	1.270	0.0004	48.5	0.0007	3.893	.00020	-0.0074
1.40	1942	0.0010	1.066	0.0004	65.4	0.0006	3.835	.00015	-0.0058
1.60	1893	0.0008	1.011	0.0001	76.8	0.0005	3.790	.00014	-0.0046
1.80	1851	0.0006	1.000	0.0000	85.3	0.0005	3.753	.00009	-0.0038
2.00	1813	0.0005	1.007	-0.0001	92.2	0.0005	3.722	.00008	-0.0032
4.00	1578	0.0000	1.281	-0.0003	126.2	0.0003	3.564	.00002	-0.0000
10.00	1303	-0.0002	2.143	-0.0004	155.8	0.0002	3.411	.00000	-0.0001
20.00	1122	-0.0002	3.342	-0.0004	172.0	0.0001	3.309	.00000	-0.0000
20.41	1117	-0.0002	3.388	-0.0004	172.4	0.0001	3.306	.00000	-0.0000
40.00	961	-0.0002	5.330	-0.0003	184.7	0.0001	3.209	.00000	-0.0000
100.00	777	-0.0002	10.066	-0.0003	197.9	0.0001	3.076	.00000	-0.0000
200.00	658	-0.0002	16.399	-0.0003	205.7	0.0000	2.979	.00000	-0.0000
400.00	554	-0.0002	26.792	-0.0003	212.0	0.0000	2.887	.00000	-0.0000
1000.00	438	-0.0002	51.338	-0.0003	218.7	0.0000	2.782	.00000	-0.0000
2000.00	365	-0.0003	83.976	-0.0003	222.6	0.0000	2.728	.00000	-0.0000
4000.00	303	-0.0003	137.439	-0.0003	225.9	0.0000	2.693	.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T_c , °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_s , (lb/sec)/ ϵ	Specific impulse exponent, n_I	Specific heat, c_p , cal/(g·°K)	$(\partial \ln M)/(\partial \ln P)_T$	$(\partial \ln M)/(\partial \ln T)_P$	
$R = 0.15$, PERCENT FUEL = 45.65, O/F = 1.190										
1.00	1183	0.0000						1.7753	0.0000	
1.05	1168	-0.0000	2.250	0.0000	47.4	0.0000	1.7710	-0.0000	-0.0000	
1.20	1129	+0.0000	1.297	+0.0000	90.8	+0.0000	1.7597	+0.0000	+0.0000	
1.40	1085	+0.0000	1.081	+0.0000	122.2	+0.0000	1.7472	+0.0000	+0.0000	
1.60	1049	+0.0000	1.018	+0.0000	143.2	+0.0000	1.7370	+0.0000	+0.0000	
1.87	1008	+0.0000	1.000	+0.0000	163.4	+0.0000	1.7256	+0.0000	+0.0000	
2.00	989	+0.0000	1.003	+0.0000	171.5	+0.0000	1.7210	+0.0000	+0.0000	
4.00	824	+0.0000	1.233	+0.0000	232.3	+0.0000	1.6824	+0.0000	+0.0000	
10.00	643	+0.0000	1.974	+0.0000	283.1	+0.0000	1.6506	+0.0000	+0.0000	
20.00	532	+0.0000	2.983	+0.0000	309.9	+0.0000	1.6345	+0.0000	+0.0000	
40.00	439	+0.0000	4.620	+0.0000	330.4	+0.0000	1.6269	+0.0000	+0.0000	
40.83	437	+0.0000	4.682	+0.0000	330.9	+0.0000	1.6267	+0.0000	+0.0000	
100.00	340	+0.0000	8.432	+0.0000	350.8	+0.0000	1.6089	+0.0000	+0.0000	
200.00	280	+0.0000	13.431	+0.0000	362.6	+0.0000	1.5951	+0.0000	+0.0000	
400.00	230	+0.0000	21.488	+0.0000	372.0	+0.0000	1.5558	+0.0000	+0.0000	
1000.00	175	+0.0000	39.928	+0.0000	381.6	+0.0000	1.4852	+0.0000	+0.0000	
2000.00	142	+0.0000	63.572	+0.0000	387.2	+0.0000	1.4387	+0.0000	+0.0000	
4000.00	114	+0.0000	100.938	+0.0000	391.6	+0.0000	1.4039	+0.0000	+0.0000	
$R = 0.20$, PERCENT FUEL = 38.65, O/F = 1.587										
1.00	1514	0.0000						1.6187	0.0000	0.0000
1.05	1497	-0.0000	2.233	0.0000	49.3	0.0000	1.6143	-0.0000	-0.0000	
1.20	1450	+0.0000	1.289	+0.0000	94.6	+0.0000	1.6024	+0.0000	+0.0000	
1.40	1398	+0.0000	1.077	+0.0000	127.4	+0.0000	1.5888	+0.0000	+0.0000	
1.60	1354	+0.0000	1.016	+0.0000	149.4	+0.0000	1.5773	+0.0000	+0.0000	
1.85	1307	+0.0000	1.000	+0.0000	169.2	+0.0000	1.5651	+0.0000	+0.0000	
2.00	1282	+0.0000	1.004	+0.0000	175.1	+0.0000	1.5584	+0.0000	+0.0000	
4.00	1079	+0.0000	1.244	+0.0000	243.2	+0.0000	1.5046	+0.0000	+0.0000	
10.00	852	+0.0000	2.009	+0.0000	297.2	+0.0000	1.4516	+0.0000	+0.0000	
20.00	709	+0.0000	3.049	+0.0000	325.9	+0.0000	1.4232	+0.0000	+0.0000	
40.00	588	+0.0000	4.739	+0.0000	346.0	+0.0000	1.4066	+0.0000	+0.0000	
40.83	585	+0.0000	4.802	+0.0000	348.6	+0.0000	1.4062	+0.0000	+0.0000	
100.00	458	+0.0000	8.679	+0.0000	370.0	+0.0000	1.3916	+0.0000	+0.0000	
200.00	379	+0.0000	13.870	+0.0000	382.7	+0.0000	1.3808	+0.0000	+0.0000	
400.00	312	+0.0000	22.296	+0.0000	393.0	+0.0000	1.3584	+0.0000	+0.0000	
1000.00	242	+0.0000	41.979	+0.0000	403.5	+0.0000	1.3402	+0.0000	+0.0000	
2000.00	198	+0.0000	67.687	+0.0000	409.7	+0.0000	1.2976	+0.0000	+0.0000	
4000.00	161	+0.0000	108.754	+0.0000	414.6	+0.0000	1.2543	+0.0000	+0.0000	
$R = 0.25$, PERCENT FUEL = 33.51, O/F = 1.984										
1.00	1817	0.0001						1.4998	0.00001	-0.0004
1.05	1797	-0.0001	2.218	0.0000	50.3	0.0000	1.4955	-0.0001	-0.0004	
1.20	1745	+0.0001	1.283	+0.0000	96.6	+0.0000	1.4840	+0.0001	-0.0003	
1.40	1686	+0.0000	1.073	+0.0000	130.1	+0.0000	1.4712	+0.0001	-0.0002	
1.60	1636	+0.0000	1.015	+0.0000	152.7	+0.0000	1.4604	+0.0000	-0.0001	
1.83	1587	+0.0000	1.000	+0.0000	171.8	+0.0000	1.4494	+0.0000	-0.0001	
2.00	1555	+0.0000	1.005	+0.0000	183.1	+0.0000	1.4423	+0.0000	-0.0001	
4.00	1322	+0.0000	1.256	+0.0000	249.3	+0.0000	1.3874	+0.0000	-0.0000	
10.00	1057	+0.0000	2.048	+0.0000	305.6	+0.0000	1.3225	+0.0000	+0.0000	
20.00	887	+0.0000	3.127	+0.0000	335.7	+0.0000	1.2849	+0.0000	+0.0000	
40.00	741	+0.0000	4.883	+0.0000	359.0	+0.0000	1.2560	+0.0000	+0.0000	
40.83	737	+0.0000	4.949	+0.0000	359.6	+0.0000	1.2552	+0.0000	+0.0000	
100.00	581	+0.0000	8.985	+0.0000	382.4	+0.0000	1.2321	+0.0000	+0.0000	
200.00	482	+0.0000	14.396	+0.0000	395.9	+0.0000	1.2189	+0.0000	+0.0000	
400.00	399	+0.0000	23.208	+0.0000	405.8	+0.0000	1.2100	+0.0000	+0.0000	
1000.00	310	+0.0000	43.893	+0.0000	418.1	+0.0000	1.1949	+0.0000	+0.0000	
2000.00	256	+0.0000	71.279	+0.0000	424.7	+0.0000	1.1810	+0.0000	+0.0000	
4000.00	210	+0.0000	115.650	+0.0000	430.2	+0.0000	1.1485	+0.0000	+0.0000	
$R = 0.30$, PERCENT FUEL = 29.57, O/F = 2.381										
1.00	2094	0.0006						1.4145	0.00010	-0.0027
1.05	2073	-0.0005	2.206	-0.0002	50.8	0.0002	1.4097	-0.0009	-0.0025	
1.20	2016	+0.0004	1.277	+0.0001	97.5	+0.0002	1.3967	+0.0007	-0.0019	
1.40	1952	+0.0003	1.071	+0.0001	131.4	+0.0002	1.3825	+0.0005	-0.0013	
1.50	1898	+0.0002	1.013	+0.0000	154.2	+0.0001	1.3706	+0.0003	-0.0010	
1.62	1847	+0.0001	1.000	+0.0000	172.7	+0.0001	1.3598	+0.0002	-0.0007	
2.00	1809	+0.0001	1.006	+0.0000	195.1	+0.0001	1.3319	+0.0002	-0.0006	
4.00	1553	+0.0000	1.266	-0.0001	252.6	+0.0001	1.2991	+0.0000	-0.0001	
10.00	1257	+0.0000	2.085	-0.0001	310.4	+0.0000	1.2336	+0.0000	+0.0000	
20.00	1064	-0.0001	3.206	+0.0000	341.7	+0.0000	1.1891	+0.0000	+0.0000	
40.83	891	-0.0001	5.106	+0.0000	366.6	+0.0000	1.1522	+0.0000	+0.0000	
40.00	895	-0.0001	5.037	+0.0000	366.0	+0.0000	1.1531	+0.0000	+0.0000	
100.00	707	-0.0001	9.324	+0.0000	390.5	+0.0000	1.1174	+0.0000	+0.0000	
200.00	590	-0.0001	14.993	+0.0000	404.8	+0.0000	1.1007	+0.0000	+0.0000	
400.00	490	-0.0001	24.234	+0.0000	416.3	+0.0000	1.0867	+0.0000	+0.0000	
1000.00	383	-0.0001	45.999	+0.0000	428.3	+0.0000	1.0746	+0.0000	+0.0000	
2000.00	317	-0.0001	74.912	+0.0000	435.4	+0.0000	1.0538	+0.0000	+0.0000	
4000.00	262	-0.0001	122.185	+0.0000	441.2	+0.0000	1.0534	+0.0000	+0.0000	

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, $T, ^\circ K$	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, $I, \text{lb/sec/lb}$	Specific-impulse exponent, n_I	Specific heat, $c_p, \text{cal/(g}^\circ\text{K)}$	$(\partial \ln M) / (\partial \ln P)_T$	$(\partial \ln M) / (\partial \ln T)_P$
$R = 0.35, \text{ PERCENT FUEL} = 26.47, \text{ O/F} = 2.778$									
1.00	2347	0.0019	2.195	0.0007	50.9	0.0007	1.3691	0.00042	-0.0101
1.05	2325	-0.0018	1.273	-0.0005	97.7	-0.0007	1.3440	-0.00039	-0.0093
1.20	2266	0.0014	1.068	0.0003	131.8	0.0006	1.3249	-0.00022	-0.0057
1.40	2198	0.0010	1.068	0.0001	154.7	0.0005	1.3099	-0.00017	-0.0044
1.60	2140	0.0008	1.012	-0.0001	172.5	0.0005	1.2974	-0.00013	-0.0035
1.81	2089	0.0006	1.000	-0.0001	185.9	0.0004	1.2874	-0.00010	-0.0028
2.00	2046	0.0004	1.007	-0.0001	254.1	0.0003	1.2291	-0.00002	-0.0006
4.00	1771	-0.0001	1.275	-0.0003	254.1	0.0003	1.2291	-0.00002	-0.0006
10.00	1451	-0.0002	2.119	-0.0003	313.0	0.0001	1.1655	-0.00000	-0.0000
20.00	1238	-0.0002	3.281	-0.0003	345.1	0.0001	1.1204	-0.00000	-0.0000
40.83	1045	-0.0002	9.260	-0.0003	370.9	0.0001	1.0783	-0.00000	-0.0000
40.00	1050	-0.0002	5.188	-0.0003	370.9	0.0001	1.0794	-0.00000	-0.0000
100.00	838	-0.0004	9.676	-0.0003	395.6	0.0001	1.0365	-0.00000	-0.0000
200.00	702	-0.0002	15.626	-0.0002	416.8	0.0000	1.0118	-0.00000	-0.0000
400.00	586	-0.0002	25.350	-0.0002	422.9	0.0000	.9953	-0.00000	-0.0000
1000.00	460	-0.0002	48.288	-0.0002	435.5	0.0000	.9789	-0.00000	-0.0000
2000.00	382	-0.0002	78.852	-0.0002	443.1	0.0000	.9692	-0.00000	-0.0000
4000.00	317	-0.0002	128.949	-0.0002	445.2	0.0000	.9590	-0.00000	-0.0000
$R = 0.40, \text{ PERCENT FUEL} = 23.95, \text{ O/F} = 3.175$									
1.00	2574	0.0046	2.184	0.0014	50.7	0.0017	1.3697	0.00120	-0.0266
1.05	2552	.0043	1.268	.0010	97.5	.0016	1.3599	.00112	-0.0250
1.20	2492	.0036	1.065	.0006	131.5	.0014	1.3344	.00091	-0.0208
1.40	2422	.0028	1.065	.0006	154.5	.0013	1.3072	.00071	-0.0167
1.60	2363	.0023	1.011	.0002	171.4	.0012	1.2856	.00057	-0.0136
1.79	2313	.0018	1.000	.0000	185.7	.0011	1.2533	.00038	-0.0095
2.00	2266	.0015	1.008	-0.0002	254.4	.0007	1.1787	.00009	-0.0025
4.00	1978	.0001	1.284	-0.0009	254.4	.0007	1.1787	-0.00009	-0.0025
10.00	1637	-0.0005	2.150	-0.0011	314.1	0.0004	1.1109	-0.00001	-0.0003
20.00	1408	-0.0005	3.351	-0.0010	346.9	0.0003	1.0669	-0.00000	-0.0000
40.00	1204	-0.0006	5.334	-0.0010	372.7	0.0002	1.0253	-0.00000	-0.0000
40.83	1199	-0.0006	5.409	-0.0010	373.4	0.0002	1.0242	-0.00000	-0.0000
100.00	970	-0.0006	10.029	-0.0009	399.1	0.0002	.9767	-0.00000	-0.0000
200.00	818	-0.0006	16.282	-0.0009	414.7	0.0001	.9478	-0.00000	-0.0000
400.00	687	-0.0006	26.525	-0.0009	427.4	0.0001	.9249	-0.00000	-0.0000
1000.00	542	-0.0006	50.761	-0.0009	440.7	0.0001	.9037	-0.00000	-0.0000
2000.00	452	-0.0006	83.105	-0.0009	448.6	0.0001	.8928	-0.00000	-0.0000
4000.00	376	-0.0006	136.261	-0.0009	455.1	0.0000	.8835	-0.00000	-0.0000
$R = 0.45, \text{ PERCENT FUEL} = 21.87, \text{ O/F} = 3.571$									
1.00	2773	0.0085	2.172	0.0021	50.4	0.0031	1.4156	0.00266	-0.0555
1.05	2752	.0081	1.263	.0015	95.9	.0029	1.4027	.00251	-0.0527
1.20	2692	.0070	1.263	.0015	130.8	.0027	1.3686	.00212	-0.0455
1.40	2624	.0059	1.063	.0009	153.7	.0025	1.3318	.00174	-0.0380
1.60	2565	.0043	1.010	.0004	169.6	.0023	1.3022	.00144	-0.0322
1.78	2517	.0043	1.000	.0000	184.9	.0022	1.2799	.00123	-0.0280
2.00	2467	.0036	1.009	-0.0004	253.7	.0015	1.2573	.00104	-0.0240
4.00	2174	.0006	1.293	-0.0020	253.7	.0015	1.1514	.00031	-0.0081
10.00	1817	-0.0008	2.182	-0.0026	314.1	0.0009	1.0682	-0.00004	-0.0112
20.00	1575	-0.0011	3.420	-0.0025	347.4	0.0007	1.0237	-0.00001	-0.0002
40.00	1357	-0.0012	5.476	-0.0024	375.8	0.0005	.9828	-0.00000	-0.0000
40.83	1350	-0.0012	5.554	-0.0024	374.5	0.0005	.9816	-0.00000	-0.0000
100.00	1104	-0.0012	10.381	-0.0024	401.0	0.0003	.9325	-0.00000	-0.0000
200.00	937	-0.0013	16.950	-0.0023	417.2	0.0003	.8996	-0.00000	-0.0000
400.00	792	-0.0013	27.755	-0.0023	430.4	0.0002	.8727	-0.00000	-0.0000
1000.00	629	-0.0014	53.398	-0.0023	444.3	0.0002	.8465	-0.00000	-0.0000
2000.00	526	-0.0014	87.714	-0.0023	452.7	0.0001	.8313	-0.00000	-0.0000
4000.00	439	-0.0014	146.197	-0.0023	459.5	0.0001	.8210	-0.00000	-0.0000
$R = 0.50, \text{ PERCENT FUEL} = 20.12, \text{ O/F} = 3.968$									
1.00	2944	0.0131	2.162	0.0026	50.0	0.0047	1.5012	0.00493	-0.0983
1.05	2923	.0127	1.258	.0019	96.1	.0044	1.4856	.00469	-0.0943
1.20	2866	.0114	1.258	.0019	129.7	.0042	1.4440	.00409	-0.0837
1.40	2800	.0099	1.061	.0012	152.5	.0039	1.3979	.00347	-0.0723
1.60	2742	.0087	1.009	.0005	167.4	.0038	1.3600	.00298	-0.0633
1.77	2699	.0078	1.000	.0000	183.5	.0036	1.3324	.00264	-0.0568
2.00	2647	.0068	1.010	-0.0006	252.4	.0026	1.1551	.00083	-0.0202
4.00	2356	.0021	1.303	-0.0032	252.4	.0026	1.1551	.00083	-0.0202
10.00	1990	-0.0010	2.216	-0.0047	313.1	0.0017	1.0408	-0.00015	-0.0041
20.00	1737	-0.0018	3.491	-0.0049	346.9	0.0012	.9888	-0.00003	-0.0009
40.00	1507	-0.0020	5.620	-0.0048	373.8	0.0009	.9482	-0.00000	-0.0001
40.83	1501	-0.0020	5.701	-0.0048	374.5	0.0009	.9471	-0.00000	-0.0001
100.00	1238	-0.0022	10.736	-0.0047	401.7	0.0007	.8984	-0.00000	-0.0000
200.00	1059	-0.0023	17.634	-0.0046	418.5	0.0005	.8634	-0.00000	-0.0000
400.00	900	-0.0023	29.032	-0.0046	432.2	0.0004	.8333	-0.00000	-0.0000
1000.00	720	-0.0024	56.203	-0.0046	446.7	0.0003	.8013	-0.00000	-0.0000
2000.00	606	-0.0023	92.675	-0.0046	452.5	0.0002	.7841	-0.00000	-0.0000
4000.00	507	-0.0025	152.844	-0.0046	462.7	0.0002	.7696	-0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area-ratio exponent, n _ε	Specific impulse, I, (lb/sec)/lb	Specific impulse exponent, n _I	Specific heat, S _c , cal/(lb·°K)	(δ ln M)/(δ ln P) _T	(δ ln M)/(δ ln T) _P
R = 3.60, PERCENT FUEL = 17.35, O/F = 4.762									
1.00	3208	0.0226	2.144	0.0028	48.8	0.0078	1.7671	0.01210	-0.2283
1.05	3189	0.0211	2.144	0.0028	48.8	0.0078	1.7482	0.01170	-0.2219
1.20	3137	0.0208	1.250	0.0021	93.8	0.0075	1.6966	0.01063	-0.2047
1.40	3077	0.0192	1.057	0.0013	126.8	0.0073	1.6375	0.00947	-0.1854
1.60	3025	0.0178	1.007	0.0005	149.1	0.0070	1.5869	0.00892	-0.1693
1.75	2990	0.0169	1.000	0.0000	162.3	0.0069	1.5531	0.00791	-0.1588
2.00	2938	0.0155	1.012	-0.0008	179.7	0.0066	1.5041	0.00705	-0.1438
4.00	2669	0.0083	1.323	-0.0048	248.0	0.0054	1.2723	0.00352	-0.0779
10.00	2313	-0.0066	2.288	-0.091	309.3	0.0039	1.0538	0.00101	-0.253
20.00	2050	-0.0027	3.644	-0.0108	343.7	0.0030	0.9574	0.00029	-0.081
40.00	1803	-0.0041	5.926	-0.0113	371.5	0.0023	0.8996	0.00006	-0.019
40.83	1796	-0.0041	6.013	-0.0113	372.3	0.0023	0.8983	0.00006	-0.019
100.00	1506	-0.0047	11.474	-0.0112	400.7	0.0017	0.8482	0.00000	-0.0002
200.00	1306	-0.0050	19.054	-0.0111	418.4	0.0013	0.8136	0.00000	-0.0000
400.00	1125	-0.0052	31.724	-0.0110	433.1	0.0011	0.7807	0.00000	-0.0000
1000.00	916	-0.0055	62.274	-0.0110	448.8	0.0008	0.7420	0.00000	-0.0003
2000.00	778	-0.0056	103.640	-0.0111	458.4	0.0007	0.7177	0.00000	-0.0000
4000.00	658	-0.0058	172.288	-0.0111	466.4	0.0005	0.6983	0.00000	-0.0000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556									
1.00	3381	0.0307	2.133	0.0024	47.4	0.0103	2.1301	0.02284	-0.4169
1.05	3364	0.0303	2.133	0.0024	47.4	0.0103	2.1115	0.02230	-0.4091
1.20	3317	0.0291	1.245	0.0018	91.2	0.0101	2.0594	0.02085	-0.3876
1.40	3263	0.0278	1.054	0.0011	123.3	0.0098	1.9976	0.01921	-0.3628
1.60	3217	0.0266	1.006	0.0004	145.2	0.0096	1.9428	0.01783	-0.3412
1.74	3188	0.0258	1.000	0.0000	157.0	0.0095	1.9085	0.01699	-0.3280
2.00	3140	0.0245	1.014	-0.0007	175.1	0.0093	1.8496	0.01600	-0.3055
4.00	2903	0.0173	1.339	-0.0047	242.3	0.0082	1.4556	0.00934	-0.2008
10.00	2584	.0070	2.356	-0.0106	303.3	0.0066	1.2090	0.00394	-0.0917
20.00	2337	.0000	3.803	-0.0147	338.3	0.0054	1.0195	0.00159	-0.003
40.00	2088	-0.0048	6.256	-0.0174	366.8	0.0043	0.9006	0.00050	-0.0139
40.83	2081	-0.0049	6.350	-0.0175	367.6	0.0043	0.8980	0.00048	-0.0135
100.00	1775	-0.0076	12.271	-0.0186	397.1	0.0092	0.8183	0.00007	-0.0023
200.00	1558	-0.0083	20.571	-0.0186	415.7	0.0026	0.7809	0.00001	-0.0004
400.00	1359	-0.0087	34.597	-0.0186	431.3	0.0021	0.7484	0.00000	-0.0001
1000.00	1125	-0.0093	68.879	-0.0186	448.2	0.0016	0.7080	0.00000	-0.0000
2000.00	968	-0.0096	115.835	-0.0187	458.6	0.0013	0.6798	0.00000	-0.0000
4000.00	828	-0.0100	194.445	-0.0188	467.4	0.0011	0.6552	0.00000	-0.0000
R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349									
1.00	3481	0.0364					2.4909	0.03537	-0.6319
1.05	3465	0.0361	2.126	0.0018	46.0	0.0119	2.4777	0.03482	-0.6249
1.20	3422	0.0352	1.242	0.0014	65.5	0.0118	2.4401	0.03330	-0.6054
1.40	3373	0.0341	1.052	0.0006	119.7	0.0116	2.3938	0.03155	-0.5818
1.60	3331	0.0332	1.008	0.0003	140.9	0.0114	2.3513	0.03003	-0.5609
1.73	3306	0.0326	1.000	0.0000	151.8	0.0113	2.3254	0.02915	-0.5485
2.00	3261	0.0316	1.015	-0.0006	170.0	0.0112	2.2752	0.02752	-0.5249
4.00	3052	0.0260	1.350	-0.0036	235.7	0.0103	2.0021	0.01991	-0.4058
10.00	2779	.0170	2.409	-0.0088	296.0	0.0090	1.5823	0.01097	-0.2447
20.00	2568	.0087	3.944	-0.0139	331.1	0.0080	1.4725	0.00579	-0.1390
40.00	2346	.0000	6.587	-0.0192	360.1	0.0068	1.0267	0.00247	-0.0641
40.83	2340	-0.0002	6.689	-0.0194	360.8	0.0068	1.0207	0.00240	-0.0625
100.00	2042	-0.0083	13.134	-0.0243	391.4	0.0023	0.8369	0.00055	-0.0124
200.00	1815	-0.0113	22.231	-0.0256	410.8	0.0043	0.7683	0.00013	-0.0041
400.00	1602	-0.0126	37.727	-0.0261	427.3	0.0035	0.7287	0.00002	-0.0008
1000.00	1347	-0.0135	76.063	-0.0262	445.3	0.0027	0.6880	0.00000	-0.0004
2000.00	1173	-0.0141	129.237	-0.0263	456.6	0.0023	0.6594	0.00000	-0.0000
4000.00	1016	-0.0147	219.200	-0.0265	466.2	0.0019	0.6320	0.00000	-0.0000
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143									
1.00	3526	0.0393					2.6656	0.04460	-0.7874
1.05	3511	0.0390	2.123	0.0015	44.5	0.0127	2.6528	0.04411	-0.7823
1.20	3469	0.0383	1.241	0.0011	55.8	0.0126	2.6432	0.04279	-0.7680
1.40	3422	0.0374	1.052	0.0006	116.1	0.0125	2.6185	0.04146	-0.7508
1.60	3382	0.0367	1.005	0.0002	159.7	0.0123	2.5953	0.03994	-0.7352
1.73	3360	0.0362	1.000	0.0000	147.0	0.0123	2.5513	0.03918	-0.7265
2.00	3317	0.0356	1.016	-0.0002	161.0	0.0121	2.5226	0.03773	-0.7087
4.00	3122	0.0314	1.356	-0.0027	228.9	0.0114	2.3586	0.03089	-0.6170
10.00	2881	.0254	2.437	-0.0061	287.9	0.0105	2.0940	0.02200	-0.4769
20.00	2705	.0199	4.032	-0.0094	321.5	0.0098	1.8100	0.01550	-0.3586
40.00	2528	.0127	6.838	-0.0138	351.5	0.0089	1.4813	0.00946	-0.2345
40.83	2523	.0125	6.947	-0.0140	352.3	0.0089	1.4712	0.00930	-0.2309
100.00	2279	-0.0001	13.977	-0.0222	383.4	0.0076	1.0541	0.00335	-0.0922
200.00	2072	-0.0095	24.037	-0.0266	403.7	0.0065	0.8410	0.00105	-0.0313
400.00	1857	-0.0149	41.251	-0.0319	421.1	0.0055	0.7376	0.00025	-0.0080
1000.00	1585	-0.0176	84.153	-0.0331	440.3	0.0043	0.6784	0.00004	-0.0007
2000.00	1397	-0.0186	144.295	-0.0333	452.5	0.0036	0.6587	0.00000	-0.0004
4000.00	1224	-0.0194	247.166	-0.0335	463.0	0.0030	0.6217	0.00000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T_c , °K	Temperature exponent, η_T	Area ratio, ϵ	Area-ratio exponent, η_ϵ	Specific impulse, I_{sp} , lb/sec/lb	Specific-impulse exponent, η_I	Specific heat, c_p , cal/g·°K	$(\delta \ln \frac{\epsilon}{P})_T$	$(\delta \ln \frac{I}{P})_T$
$R = 1.00$, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3534	0.0399					2.6053	0.04709	-0.8301
1.05	3519	0.0396	2.122	0.0014	43.3	0.0129	2.6007	0.04664	-0.8258
1.20	3478	0.0389	1.240	0.0010	83.3	0.0128	2.5874	0.04541	-0.8135
1.40	3431	0.0381	1.051	0.0006	112.7	0.0126	2.5703	0.04399	-0.7989
1.60	3392	0.0374	1.005	0.0002	132.7	0.0125	2.5542	0.04277	-0.7857
1.73	3370	0.0370	1.000	0.0000	142.7	0.0124	2.5445	0.04208	-0.7781
2.00	3327	0.0363	1.016	-0.0004	160.1	0.0123	2.5243	0.04073	-0.7630
4.00	3137	0.0327	1.357	-0.0024	222.3	0.0117	2.4094	0.03451	-0.6863
10.00	2903	0.0277	2.6445	-0.0053	279.6	0.0108	2.2079	0.02666	-0.5732
20.00	2738	0.0236	4.055	-0.0077	313.3	0.0104	2.0416	0.02111	-0.4817
40.00	2578	0.0192	6.910	-0.0103	341.7	0.0096	1.8120	0.01600	-0.3879
40.83	2573	0.0190	7.022	-0.0104	342.5	0.0095	1.8056	0.01585	-0.3851
100.00	2371	0.0123	14.326	-0.0146	373.2	0.0087	1.5117	0.01011	-0.2667
200.00	2214	0.0061	25.124	-0.0186	393.6	0.0080	1.2810	0.00647	-0.1829
400.00	2052	-0.0011	4.210	-0.0235	411.4	0.0074	1.0554	0.00366	-0.1117
1000.00	1826	-0.0112	93.124	-0.0305	431.8	0.0064	0.8338	0.00132	-0.0452
2000.00	1648	-0.0177	162.695	-0.0352	445.0	0.0053	0.7163	0.00047	-0.0177
4000.00	1470	-0.0220	282.648	-0.0381	456.5	0.0045	0.6444	0.00013	-0.0053
$R = 1.50$, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3374	0.0324	1.242	0.0013	73.5	0.0107	1.5942	0.02714	-0.5145
1.20	3315	0.0312	2.125	0.0017	38.2	0.0109	1.6157	0.02553	-0.4930
1.40	3358	0.0321	2.125	0.0017	38.2	0.0106	1.5682	0.02418	-0.4745
1.60	3267	0.0302	1.052	0.0007	99.4	0.0104	1.5447	0.02304	-0.4583
1.73	3202	0.0288	1.000	0.0000	117.1	0.0103	1.5306	0.02237	-0.4488
2.00	3158	0.0278	1.015	-0.0005	141.5	0.0104	1.5034	0.02115	-0.4308
4.00	2953	0.0230	1.351	-0.0032	197.9	0.0094	1.3606	0.01566	-0.3433
10.00	2692	0.0158	2.6415	-0.0073	266.1	0.0083	1.1474	0.00942	-0.2294
20.00	2496	0.0097	3.967	-0.0110	275.3	0.0074	0.9816	0.00569	-0.1516
40.00	2297	0.0034	6.664	-0.0151	299.5	0.0062	0.8274	0.00298	-0.0879
40.83	2291	0.0030	6.768	-0.0152	300.2	0.0065	0.8232	0.00292	-0.0865
100.00	2026	-0.0048	13.428	-0.0204	326.0	0.0053	0.6882	0.00095	-0.0348
200.00	1818	-0.0091	24.891	-0.0229	342.6	0.0044	0.5904	0.00031	-0.0143
400.00	1616	-0.0115	39.039	-0.0243	356.7	0.0036	0.5432	0.00008	-0.0037
1000.00	1366	-0.0130	79.054	-0.0249	372.3	0.0026	0.4048	0.00001	-0.0005
2000.00	1193	-0.0137	134.733	-0.0251	382.1	0.0024	0.4834	0.00000	-0.0001
4000.00	1039	-0.0143	229.310	-0.0253	390.4	0.0020	0.4636	0.00000	-0.0000
$R = 2.00$, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	3158	0.0243					1.1081	0.01418	-0.2964
1.05	3141	0.0240	2.132	0.0020	34.9	0.0086	1.1005	0.01385	-0.2912
1.20	3097	0.0230	1.245	0.0015	67.1	0.0085	1.0794	0.01296	-0.2770
1.40	3046	0.0219	1.054	0.0009	90.8	0.0083	1.0543	0.01197	-0.2606
1.60	3002	0.0209	1.006	0.0003	108.9	0.0081	1.0320	0.01114	-0.2463
1.73	2975	0.0203	1.000	0.0000	115.5	0.0080	1.0182	0.01064	-0.2379
2.00	2929	0.0192	1.014	-0.0006	128.9	0.0078	0.9940	0.00980	-0.2234
4.00	2706	0.0137	1.341	-0.0037	178.4	0.0069	0.8720	0.00619	-0.1546
10.00	2413	0.0061	2.365	-0.0083	223.5	0.0056	0.7166	0.00278	-0.0797
20.00	2189	0.0008	3.829	-0.0115	249.4	0.0047	0.6182	0.00125	-0.0405
40.00	1965	-0.0032	6.321	-0.0140	270.5	0.0038	0.5459	0.00046	-0.0170
40.83	1959	-0.0033	6.416	-0.0141	271.1	0.0036	0.5441	0.00045	-0.0166
100.00	1678	-0.0062	12.437	-0.0156	293.1	0.0029	0.4875	0.00009	-0.0039
200.00	1475	-0.0072	20.879	-0.0160	307.0	0.0023	0.4613	0.00002	-0.0010
400.00	1287	-0.0076	35.155	-0.0160	318.7	0.0019	0.4417	0.00000	-0.0002
1000.00	1070	-0.0081	70.143	-0.0160	331.3	0.0014	0.4194	0.00000	-0.0000
2000.00	923	-0.0084	118.235	-0.0161	339.2	0.0012	0.4040	0.00000	-0.0000
4000.00	792	-0.0087	199.011	-0.0162	345.8	0.0010	0.3894	0.00000	-0.0000
$R = 3.00$, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2747	0.0120					0.6509	0.00385	-0.0973
1.05	2729	0.0117	2.152	0.0022	30.6	0.0046	0.6451	0.00369	-0.0940
1.20	2679	0.0107	1.254	0.0016	58.8	0.0044	0.6293	0.00328	-0.0853
1.40	2622	0.0096	1.058	0.0009	79.4	0.0042	0.6114	0.00284	-0.0758
1.60	2573	0.0085	1.008	0.0004	93.4	0.0040	0.5963	0.00249	-0.0680
1.73	2538	0.0079	1.000	0.0000	102.1	0.0039	0.5858	0.00246	-0.0626
2.00	2491	0.0071	1.011	-0.0005	112.5	0.0037	0.5720	0.00197	-0.0561
4.00	2237	0.0029	1.314	-0.0030	159.0	0.0029	0.5059	0.00085	-0.0275
10.00	1913	-0.0005	2.253	-0.0020	192.9	0.0020	0.4460	0.00021	-0.0087
20.00	1682	-0.0017	3.569	-0.0055	214.0	0.0015	0.4185	0.00005	-0.0025
40.00	1470	-0.0022	5.778	-0.0056	231.0	0.0011	0.4000	0.00001	-0.0006
40.83	1464	-0.0022	5.862	-0.0055	231.4	0.0011	0.3995	0.00001	-0.0006
100.00	1220	-0.0024	11.130	-0.0055	248.7	0.0008	0.3811	0.00000	-0.0001
200.00	1053	-0.0025	18.422	-0.0055	259.4	0.0006	0.3679	0.00000	-0.0000
400.00	904	-0.0026	30.593	-0.0054	268.3	0.0005	0.3555	0.00000	-0.0000
1000.00	733	-0.0027	59.908	-0.0054	277.8	0.0004	0.3398	0.00000	-0.0000
2000.00	622	-0.0028	94.545	-0.0054	285.5	0.0003	0.3290	0.00000	-0.0000
4000.00	525	-0.0029	165.173	-0.0053	286.3	0.0003	0.3194	0.00000	-0.0000

TABLE III. - Concluded. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P_e/P	Temperature, T_e , °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_{sp} , lb/sec/b	Specific-impulse exponent, n_I	Specific heat, c_p , cal/(g·°K)	$(\partial \ln R) / (\partial \ln P)_T$	$(\partial \ln R) / (\partial \ln T)_P$
$R = 4.00$, PERCENT FUEL = 3.05, C/F = 1.746									
1.00	2381	0.0046						0.4697	0.00095
1.05	2362	0.0044	2.174	0.0013	27.6	0.0019	0.4663	0.00089	-0.0288
1.20	2309	0.0038	1.263	0.0009	53.0	0.017	0.4572	0.00075	-0.0274
1.40	2249	0.0031	1.063	0.0005	71.5	0.016	0.4473	0.00060	-0.0196
1.60	2198	0.0026	1.010	0.0002	84.0	0.015	0.4393	0.00050	-0.0166
1.78	2157	0.0022	1.000	0.0000	92.8	0.014	0.4332	0.00042	-0.0145
2.00	2113	0.0018	1.009	-0.0002	101.1	0.013	0.4272	0.00035	-0.0124
4.00	1860	0.0003	1.293	-0.0011	138.7	0.009	0.3982	0.0011	-0.0044
10.00	1554	-0.0005	2.182	-0.0015	171.6	0.0035	0.3743	0.00002	-0.0008
20.00	1348	-0.0006	3.423	-0.0015	149.8	0.0034	0.3612	0.00000	-0.0002
40.00	1164	-0.0007	5.493	-0.0014	204.3	0.0033	0.3499	0.00000	0.0000
40.83	1159	-0.0007	5.572	-0.0014	204.7	0.0033	0.3495	0.00000	0.0000
100.00	952	-0.0007	10.461	-0.0014	219.2	0.002	0.3352	0.00000	0.0000
200.00	813	-0.0007	17.162	-0.0013	228.2	0.002	0.3243	0.00000	0.0000
400.00	690	-0.0008	28.237	-0.0013	235.5	0.001	0.3139	0.00000	0.0000
1000.00	551	-0.0008	54.608	-0.0013	243.3	0.001	0.3012	0.00000	0.0000
2000.00	463	-0.0008	89.893	-0.0013	247.9	0.001	0.2927	0.00000	0.0000
4000.00	386	-0.0008	147.835	-0.0013	251.8	0.001	0.2864	0.00000	0.0000
$R = 5.00$, PERCENT FUEL = 2.45, C/F = 9.683									
1.00	2072	0.0015						0.3924	0.00022
1.05	2053	0.014	2.190	0.0005	25.2	0.0106	0.3905	0.00020	-0.0074
1.20	2002	0.011	1.270	0.0004	48.5	0.0106	0.3859	0.00016	-0.0061
1.40	1944	0.008	1.067	0.0002	65.4	0.0105	0.3808	0.00012	-0.0044
1.60	1894	0.007	1.011	0.0001	76.8	0.0104	0.3767	0.00010	-0.0036
1.80	1852	0.005	1.000	0.0000	85.3	0.0104	0.3734	0.00008	-0.0032
2.00	1813	0.004	1.007	-0.0001	92.3	0.0104	0.3706	0.00006	-0.0026
4.00	1578	0.0000	1.281	-0.0003	126.2	0.0102	0.3559	0.00001	-0.0007
10.00	1303	-0.0002	2.143	-0.0003	155.8	0.0101	0.3410	0.00000	-0.0001
20.00	1122	-0.0002	3.341	-0.0003	172.0	0.0101	0.3309	0.00000	0.0000
40.00	961	-0.0002	5.329	-0.0003	184.7	0.0101	0.3209	0.00000	0.0000
40.83	956	-0.0002	5.405	-0.0003	185.1	0.0101	0.3206	0.00000	0.0000
100.00	777	-0.0002	10.063	-0.0003	197.9	0.0100	0.3076	0.00000	0.0000
200.00	658	-0.0002	16.396	-0.0003	205.7	0.0100	0.2979	0.00000	0.0000
400.00	554	-0.0002	26.787	-0.0003	212.0	0.0100	0.2887	0.00000	0.0000
1000.00	438	-0.0002	51.327	-0.0003	218.7	0.0100	0.2782	0.00000	0.0000
2000.00	365	-0.0002	83.959	-0.0003	222.6	0.0100	0.2728	0.00000	0.0000
4000.00	303	-0.0002	137.411	-0.0003	225.9	0.0100	0.2693	0.00000	0.0000

TABLE IV. - EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN
AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Combustion-chamber pressure, 60 pounds per square inch absolute

R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190															
Pressure, lb/sq in. abs Temperature, °K	60.00 1183	50.00 1129	42.86 1035	37.50 1049	32.17 1008	15.00 824	14.70 819	6.00 643	3.00 532	1.50 439	0.60 340	0.30 280	0.06 175	0.03 142	
H ₂ H ₂ O	0.85000 +15000	0.85000 +15000													
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587															
Pressure, lb/sq in. abs Temperature, °K	60.00 1514	50.00 1450	42.86 1398	37.50 1354	32.17 1307	15.00 1079	14.70 1073	6.00 852	3.00 709	1.50 588	0.60 458	0.30 379	0.06 242	0.03 198	
H H ₂ H ₂ O	0.00001 +7999 +20000	0.00000 +80000 +20000	0.00000 +80000 +20000												
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984															
Pressure, lb/sq in. abs Temperature, °K	60.00 1816	50.00 1744	42.86 1686	37.50 1636	32.17 1507	15.00 1322	14.70 1316	6.00 1057	3.00 887	1.50 741	0.60 581	0.30 482	0.06 310	0.03 256	
H H ₂ H ₂ O	0.00017 +74985 +24997	0.00010 +74991 +24998	0.00006 +74996 +24999	0.00004 +74998 +25000	0.00003 +75000 +25000	0.00000 +75000 +25000	0.00000 +75000 +25000	0.00000 +75000 +25000							
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381															
Pressure, lb/sq in. abs Temperature, °K	60.00 2089	50.00 2013	42.86 1950	37.50 1896	32.17 1846	15.00 1553	14.70 1546	6.00 1258	3.00 1064	1.50 896	0.60 708	0.30 590	0.06 383	0.03 317	
H H ₂ H ₂ O OH	0.00120 +69899 +29975 +0.0006	0.00080 +69932 +29984 +0.0004	0.00040 +69953 +29989 +0.0002	0.00029 +69966 +29992 +0.0001	0.00023 +69976 +29995 +0.0001	0.00003 +69978 +29998 +0.0000	0.00003 +69998 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	0.00000 +70000 +30000 +0.0000	
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.776															
Pressure, lb/sq in. abs Temperature, °K	60.00 2329	50.00 2253	42.86 2189	37.50 2133	32.17 2085	15.00 1772	14.70 1764	6.00 1452	3.00 1239	1.50 1051	0.60 838	0.30 703	0.06 560	0.03 382	
H H ₂ H ₂ O OH	0.00446 +64540 +34873 +0.0041	0.00328 +64735 +34734 +0.0027	0.00248 +64844 +34854 +0.0019	0.00192 +64877 +34851 +0.0013	0.00150 +64877 +34862 +0.0010	0.00022 +64982 +34995 +0.0001	0.00021 +64983 +34996 +0.0000	0.00001 +64999 +35000 +0.0000	0.00000 +65000 +35000 +0.0000	0.00000 +65000 +35000 +0.0000	0.00000 +65000 +35000 +0.0000	0.00000 +65000 +35000 +0.0000	0.00000 +65000 +35000 +0.0000	0.00000 +65000 +35000 +0.0000	
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175															
Pressure, lb/sq in. abs Temperature, °K	60.00 2531	50.00 2458	42.86 2396	37.50 2342	32.17 2298	15.00 1978	14.70 1970	6.00 1640	3.00 1411	1.50 1207	0.60 972	0.30 820	0.06 543	0.03 453	
H O H ₂ H ₂ O O ₂ OH	0.01092 +59160 +39584 +0.0001	0.00867 +59331 +39583 +0.0000	0.00702 +59456 +39583 +0.0000	0.00577 +59552 +39602 +0.0000	0.00488 +59621 +39637 +0.0000	0.00106 +59616 +39637 +0.0000	0.00102 +59700 +39707 +0.0000	0.00010 +59792 +39797 +0.0000	0.00001 +59992 +39998 +0.0000	0.00000 +60000 +40000 +0.0000	0.00000 +60000 +40000 +0.0000	0.00000 +60000 +40000 +0.0000	0.00000 +60000 +40000 +0.0000	0.00000 +60000 +40000 +0.0000	
R = 0.45, PERCENT FUEL = 21.57, O/F = 3.571															
Pressure, lb/sq in. abs Temperature, °K	60.00 2695	50.00 2628	42.86 2570	37.50 2519	32.17 2481	15.00 2167	14.70 2159	6.00 1822	3.00 1551	1.50 1362	0.60 1109	0.30 942	0.06 632	0.03 529	
H O H ₂ H ₂ O O ₂ OH	0.02118 +55446 +34899 +0.0003	0.01599 +53767 +44183 +0.0002	0.01451 +53342 +44326 +0.0002	0.01253 +54053 +44456 +0.0001	0.01115 +54161 +44745 +0.0001	0.00340 +54754 +44877 +0.0001	0.00328 +54982 +44985 +0.0001	0.00050 +54992 +44998 +0.0001	0.00005 +54999 +45000 +0.0001	0.00000 +55000 +45000 +0.0000	0.00000 +55000 +45000 +0.0000	0.00000 +55000 +45000 +0.0000	0.00000 +55000 +45000 +0.0000	0.00000 +55000 +45000 +0.0000	
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968															
Pressure, lb/sq in. abs Temperature, °K	60.00 2828	50.00 2765	42.86 2711	37.50 2664	32.17 2594	15.00 2335	14.70 2327	6.00 1996	3.00 1748	1.50 1518	0.60 1247	0.30 1067	0.06 727	0.03 611	
H O H ₂ H ₂ O O ₂ OH	0.00777 +50036 +47961 +0.0005	0.02700 +50026 +48192 +0.0004	0.02492 +50020 +48304 +0.0003	0.02151 +50013 +48506 +0.0003	0.01985 +50013 +48506 +0.0003	0.00401 +50020 +48506 +0.0003	0.00770 +50474 +48877 +0.0003	0.00174 +50474 +48877 +0.0003	0.00035 +50492 +48985 +0.0003	0.00005 +50499 +49000 +0.0003	0.00000 +50500 +49000 +0.0003	0.00000 +50500 +49000 +0.0003	0.00000 +50500 +49000 +0.0003	0.00000 +50500 +49000 +0.0003	
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762															
Pressure, lb/sq in. abs Temperature, °K	60.00 3015	50.00 2961	42.86 2914	37.50 2874	32.17 2849	15.00 2595	14.70 2587	6.00 2299	3.00 2051	1.50 1829	0.60 1518	0.30 1247	0.06 954	0.03 792	
H O H ₂ H ₂ O O ₂ OH	0.00998 +55592 +37569 +0.00119	0.04628 +50167 +37609 +0.00119	0.04316 +50141 +37619 +0.00119	0.04048 +50121 +37619 +0.00119	0.03984 +50093 +37619 +0.00119	0.02303 +50091 +38063 +0.00119	0.02257 +50091 +38063 +0.00119	0.00943 +50091 +38063 +0.00119	0.00363 +50091 +38063 +0.00119	0.00087 +50091 +38063 +0.00119	0.00004 +50091 +38063 +0.00119	0.00001 +50091 +38063 +0.00119	0.00000 +50091 +38063 +0.00119		
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556															
Pressure, lb/sq in. abs Temperature, °K	60.00 3128	50.00 3076	42.86 3037	37.50 2981	32.17 2961	15.00 2761	14.70 2757	6.00 2517	3.00 2320	1.50 2108	0.60 1813	0.30 1596	0.06 1156	0.03 996	
H O H ₂ H ₂ O O ₂ OH	0.00575 +55592 +36862 +0.00441	0.05732 +50025 +36857 +0.00441	0.05300 +50025 +36857 +0.00441	0.05130 +50025 +36857 +0.00441	0.03770 +50025 +36857 +0.00441	0.02275 +50025 +36857 +0.00441	0.01282 +50025 +36857 +0.00441	0.00555 +50025 +36857 +0.00441	0.00108 +50025 +36857 +0.00441	0.00040 +50025 +36857 +0.00441	0.00000 +50025 +36857 +0.00441	0.00000 +50025 +36857 +0.00441	0.00000 +50025 +36857 +0.00441		

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute

R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349															
Pressure, lb/sq in. abs Temperature, °K	60.00 3168	50.00 3141	42.86 3123	37.50 3076	34.86 3024	15.00 2653	14.70 2648	6.00 2645	3.00 2641	1.50 2641	0.60 2674	0.30 2674	0.06 1598	0.03 1220	
H	0.06315	0.05603	0.05851	0.05688	0.05253	0.04433	0.04476	0.03427	0.02537	0.01471	0.00281	0.00193	0.00003	0.00000	
O	0.1163	0.1075	0.1003	0.0943	0.0910	0.0574	0.0574	0.0574	0.0492	0.04142	0.00000	0.00000	0.00000	0.00000	
H ₂	0.2260	0.2204	0.1933	0.1594	0.1734	0.0957	0.0959	0.1140	0.1950	0.19785	0.17742	0.19710	0.19956	0.20000	
H ₂ O	0.6203	0.6297	0.3747	0.6492	0.6471	0.0593	0.0593	0.0593	0.75565	0.77672	0.79340	0.79834	0.79958	0.80000	
O ₂	0.1305	0.1237	0.1178	0.1127	0.1079	0.0771	0.0763	0.0635	0.0226	0.00044	0.0010	0.0001	0.00000	0.00000	
OH	0.0695	0.0695	0.06301	0.0626	0.05922	0.04422	0.04507	0.04501	0.01667	0.0002	0.00273	0.00061	0.00000	0.00000	
R = 0.90, PERCENT FUEL = 12.26, O/F = 7.143															
Pressure, lb/sq in. abs Temperature, °K	60.00 3213	50.00 3168	42.86 3124	37.50 3076	34.86 3024	15.00 2692	14.70 2686	6.00 2674	3.00 2671	1.50 2671	0.60 2646	0.30 2646	0.06 1660	0.03 1408	
H	0.05966	0.05741	0.05554	0.05392	0.05306	0.04322	0.04295	0.03322	0.02615	0.01179	0.00671	0.00049	0.00008	0.00000	
O	0.11787	0.1186	0.11502	0.10531	0.10493	0.01084	0.01074	0.00708	0.00747	0.00107	0.00342	0.00000	0.00000	0.00000	
H ₂	0.17295	0.17043	0.16860	0.1660	0.1650	0.13516	0.13516	0.13516	0.12460	0.12191	0.10760	0.10202	0.09483	0.09493	
H ₂ O	0.63334	0.64519	0.55350	0.56058	0.56474	0.70441	0.70441	0.70441	0.71114	0.82334	0.86120	0.86268	0.8948	0.89793	
O ₂	0.12642	0.12572	0.12511	0.12427	0.12427	0.02046	0.02038	0.01533	0.00828	0.00362	0.01210	0.00000	0.00000	0.00000	
OH	0.08775	0.08430	0.08156	0.07512	0.07782	0.0287	0.0287	0.0452	0.03665	0.02648	0.01445	0.00704	0.00021	0.00002	
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937															
Pressure, lb/sq in. abs Temperature, °K	60.00 3217	50.00 3173	42.86 3124	37.50 3104	34.86 3060	15.00 2700	14.70 2696	6.00 2676	3.00 2671	1.50 2671	0.60 2671	0.30 2671	0.06 1740	0.03 1414	
H	0.05355	0.05143	0.04967	0.04817	0.04736	0.03825	0.03804	0.02142	0.02281	0.01710	0.01061	0.00667	0.00115	0.00032	
O	0.1347	0.1234	0.1214	0.12061	0.12019	0.11555	0.11555	0.11555	0.11446	0.1117	0.08554	0.07274	0.06339	0.00194	
H ₂	0.13620	0.13400	0.13100	0.12771	0.12771	0.11406	0.11406	0.11406	0.11272	0.10941	0.061010	0.07346	0.06844	0.04354	
H ₂ O	0.64117	0.65113	0.56953	0.56681	0.567071	0.71636	0.71636	0.71636	0.71746	0.76019	0.83610	0.88022	0.91123	0.98976	
O ₂	0.04445	0.04394	0.04306	0.04266	0.04266	0.02983	0.02983	0.02983	0.03723	0.02602	0.02453	0.01773	0.00708	0.00328	
OH	0.10118	0.09776	0.09490	0.09243	0.09111	0.07592	0.07592	0.06042	0.04942	0.03917	0.02693	0.01986	0.00227	0.00243	
R = 1.50, PERCENT FUEL = 7.749, O/F = 1.905															
Pressure, lb/sq in. abs Temperature, °K	60.00 3116	50.00 3070	42.86 3031	37.50 2994	34.86 2951	15.00 2782	14.70 2777	6.00 2776	3.00 2771	1.50 2771	0.60 2640	0.30 2640	0.06 1856	0.03 1410	
H	0.02428	0.02275	0.02149	0.02042	0.01985	0.01367	0.01353	0.00808	0.00476	0.00237	0.00061	0.00013	0.00000	0.00000	
O	0.03338	0.03164	0.03019	0.02985	0.02895	0.02692	0.02692	0.02692	0.02675	0.02184	0.02142	0.01916	0.00663	0.00001	
H ₂	0.04909	0.04690	0.04501	0.04344	0.04257	0.03260	0.03236	0.0231	0.01523	0.00915	0.00341	0.00112	0.00002	0.00000	
H ₂ O	0.61197	0.62046	0.57576	0.57372	0.57293	0.67453	0.67453	0.67453	0.71424	0.70686	0.78293	0.79298	0.79597	0.80000	
O ₂	0.16807	0.16933	0.17043	0.17144	0.17193	0.17167	0.17167	0.17167	0.18750	0.19134	0.19500	0.19732	0.19988	0.20000	
OH	0.11322	0.10887	0.10520	0.10204	0.10031	0.08062	0.08013	0.05187	0.04493	0.03104	0.01549	0.00721	0.00061	0.00007	
R = 2.00, PERCENT FUEL = 5.927, O/F = 5.873															
Pressure, lb/sq in. abs Temperature, °K	60.00 2966	50.00 2917	42.86 2877	37.50 2841	34.86 2821	15.00 2604	14.70 2599	6.00 2595	3.00 2579	1.50 2579	0.60 1705	0.30 1705	0.06 1059	0.03 945	
H	0.01009	0.00913	0.00837	0.00770	0.00734	0.00395	0.00388	0.0052	0.00054	0.00013	0.00001	0.00000	0.00000	0.00000	
O	0.02669	0.02468	0.02302	0.02162	0.02083	0.01978	0.01978	0.01978	0.01950	0.01821	0.01011	0.00015	0.00004	0.00000	
H ₂	0.02078	0.01933	0.01812	0.01709	0.01651	0.01053	0.01040	0.01040	0.01247	0.02449	0.00888	0.00414	0.00042	0.00000	
H ₂ O	0.55950	0.56635	0.57202	0.57941	0.57960	0.60805	0.60805	0.60805	0.63197	0.64800	0.65667	0.66479	0.66621	0.66666	
O ₂	0.09223	0.09473	0.09661	0.09627	0.09593	0.10000	0.10100	0.10100	0.10740	0.10927	0.10927	0.10927	0.10927	0.10927	
OH	0.09071	0.08579	0.08165	0.07610	0.07600	0.05447	0.05396	0.03103	0.01922	0.00734	0.00250	0.00064	0.00001	0.00006	
R = 3.00, PERCENT FUEL = 4.031, O/F = 3.810															
Pressure, lb/sq in. abs Temperature, °K	60.00 2655	50.00 2599	42.86 2570	37.50 2504	34.86 2481	15.00 2216	14.70 2209	6.00 2115	3.00 1691	1.50 1691	0.60 1480	0.30 1480	0.06 1061	0.03 827	
H	0.00150	0.00122	0.00100	0.00084	0.00074	0.00018	0.00017	0.00012	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	
O	0.01000	0.00863	0.00745	0.00652	0.00595	0.00206	0.00137	0.00066	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	
H ₂	0.00406	0.00348	0.00303	0.00267	0.00244	0.00087	0.00085	0.00085	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	
H ₂ O	0.64003	0.64616	0.47142	0.47420	0.47593	0.48011	0.48011	0.48011	0.49740	0.49944	0.49944	0.49944	0.49944	0.49944	
O ₂	0.47702	0.47971	0.46165	0.46561	0.46573	0.46573	0.46573	0.46573	0.49100	0.49944	0.49944	0.49944	0.49944	0.49944	
OH	0.04329	0.03583	0.03519	0.03215	0.03020	0.01476	0.01445	0.00107	0.00144	0.00033	0.00000	0.00000	0.00000	0.00000	
R = 4.00, PERCENT FUEL = 3.054, O/F = 1.746															
Pressure, lb/sq in. abs Temperature, °K	60.00 2347	50.00 2262	42.86 2228	37.50 2180	34.86 2143	15.00 1656	14.70 1651	6.00 1556	3.00 1521	1.50 1521	0.60 1477	0.30 1477	0.06 0121	0.03 0044	
H	0.00015	0.00011	0.00008	0.00006	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
O	0.00245	0.00165	0.00144	0.00114	0.00094	0.00016	0.00115	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.00068	0.00052	0.00041	0.00037	0.00027	0.00005	0.00024	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂ O	0.58920	0.59447	0.39447	0.39523	0.39523	0.39883	0.39883	0.39883	0.49650	0.55704	0.55704	0.55704	0.55704	0.55704	0.55704
O ₂	0.55176	0.55176	0.35176	0.35176	0.35176	0.35215	0.35215	0.35215	0.49511	0.49511	0.49511	0.49511	0.49511	0.49511	0.49511
OH	0.15429	0.11321	0.01112	0.01125	0.00840	0.00255	0.00247	0.00042	0.00042	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000
R = 5.00, PERCENT FUEL = 2.458, O/F = 5.683															
Pressure, lb/sq in. abs Temperature, °K	60.00 2262	50.00 1955	42.86 1949	37.50 1847	34.86 1										

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR
LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Combustion-chamber pressure, 150 pounds per square inch absolute

$R = 0.15$, PERCENT FUEL = 45.65, O/F = 1.190																
Pressure, lb/sq in. abs Temperature, °K	150.00 1183	125.00 1129	107.14 1085	93.75 1049	80.42 1008	37.50 824	15.00 643	14.70 639	7.50 592	3.75 439	1.50 340	0.75 280	0.15 175	0.08 142		
H ₂ H ₂ O	0.85000 +15000															
$R = 0.20$, PERCENT FUEL = 38.65, O/F = 1.587																
Pressure, lb/sq in. abs Temperature, °K	150.00 1514	125.00 1450	107.14 1398	93.75 1354	81.24 1307	37.50 1079	15.00 552	14.70 847	7.50 709	3.75 588	1.50 458	0.75 379	0.15 242	0.08 198		
H H ₂ H ₂ O	0.00001 +79999 +20000	0.00000 +80000 +20000														
$R = 0.25$, PERCENT FUEL = 33.51, O/F = 1.984																
Pressure, lb/sq in. abs Temperature, °K	150.00 1816	125.00 1745	107.14 1686	93.75 1636	81.96 1587	37.50 1322	15.00 1057	14.70 1052	7.50 887	3.75 741	1.50 581	0.75 482	0.15 310	0.08 226		
H H ₂ H ₂ O	0.00001 +74990 +24998	0.00007 +74994 +24999	0.00004 +74996 +24999	0.00003 +74998 +25000	0.00002 +75000 +25000	0.00000 +75000 +25000	0.00000 +75000 +25000									
$R = 0.30$, PERCENT FUEL = 29.57, O/F = 2.381																
Pressure, lb/sq in. abs Temperature, °K	150.00 2092	125.00 2015	107.14 1951	93.75 1897	82.58 1846	37.50 1553	15.00 1298	14.70 1251	7.50 1064	3.75 895	1.50 708	0.75 590	0.15 383	0.08 317		
H H ₂ H ₂ O OH	0.00077 +69935 +29984 +0.0004	0.00051 +69957 +29990 +0.0002	0.00036 +69970 +29995 +0.0001	0.00026 +69978 +29995 +0.0001	0.00018 +69984 +29997 +0.0001	0.00002 +69999 +30000 +0.0000	0.00000 +70000 +30000 +0.0000									
$R = 0.35$, PERCENT FUEL = 26.47, O/F = 2.778																
Pressure, lb/sq in. abs Temperature, °K	150.00 2339	125.00 2259	107.14 2193	93.75 2137	83.19 2137	37.50 2172	15.00 1451	14.70 1444	7.50 1239	3.75 1011	1.50 838	0.75 702	0.15 460	0.08 382		
H H ₂ H ₂ O OH	0.00296 +64761 +34915 +0.0028	0.00215 +64826 +34915 +0.0018	0.00161 +64889 +34957 +0.0009	0.00124 +64859 +34968 +0.0009	0.00097 +64921 +34976 +0.0008	0.00014 +64988 +34997 +0.0000	0.00001 +65000 +35000 +0.0000	0.00001 +65000 +35000 +0.0000	0.00000 +65000 +35000 +0.0000							
$R = 0.40$, PERCENT FUEL = 23.95, O/F = 3.175																
Pressure, lb/sq in. abs Temperature, °K	150.00 2553	125.00 2475	107.14 2410	93.75 2353	83.84 2306	37.50 1978	15.00 1636	14.70 1631	7.50 1410	3.75 1206	1.50 971	0.75 819	0.15 543	0.08 452		
H O H ₂ H ₂ O OH	0.00758 +59915 +29918 +37079 +0.0115	0.00593 +59935 +29943 +39782 +0.0082	0.00474 +59953 +29963 +39832 +0.0061	0.00386 +59970 +29981 +39867 +0.0046	0.00326 +59972 +29984 +39868 +0.0036	0.00057 +59987 +30000 +40000 +0.0004	0.00006 +59997 +30000 +40000 +0.0000	0.00006 +59999 +30000 +40000 +0.0000	0.00001 +60000 +30000 +40000 +0.0001	0.00000 +60000 +30000 +40000 +0.0000	0.00000 +60000 +30000 +40000 +0.0000	0.00000 +60000 +30000 +40000 +0.0000	0.00000 +60000 +30000 +40000 +0.0000	0.00000 +60000 +30000 +40000 +0.0000	0.00000 +60000 +30000 +40000 +0.0000	
$R = 0.45$, PERCENT FUEL = 21.87, O/F = 3.571																
Pressure, lb/sq in. abs Temperature, °K	150.00 2733	125.00 2659	107.14 2590	93.75 2542	84.52 2499	37.50 2171	15.00 1819	14.70 1812	7.50 1578	3.75 1354	1.50 1106	0.75 939	0.15 631	0.08 528		
H O H ₂ H ₂ O O ₂ OH	0.01469 +50006 +55941 +44255 +0.0002	0.01217 +50004 +54117 +44408 +0.0002	0.01025 +50002 +54253 +44420 +0.0002	0.00875 +50000 +54360 +44603 +0.0001	0.00768 +50000 +54436 +44660 +0.0001	0.00220 +50000 +54835 +44920 +0.0000	0.00031 +50000 +54977 +44991 +0.0000	0.00029 +50000 +54978 +44991 +0.0000	0.00004 +50000 +55000 +45000 +0.0000	0.00000 +50000 +55000 +45000 +0.0000	0.00000 +50000 +55000 +45000 +0.0000	0.00000 +50000 +55000 +45000 +0.0000	0.00000 +50000 +55000 +45000 +0.0000	0.00000 +50000 +55000 +45000 +0.0000	0.00000 +50000 +55000 +45000 +0.0000	
$R = 0.50$, PERCENT FUEL = 20.12, O/F = 3.968																
Pressure, lb/sq in. abs Temperature, °K	150.00 2881	125.00 2811	107.14 2752	93.75 2701	85.15 2664	37.50 2346	15.00 1994	14.70 1986	7.50 1743	3.75 1512	1.50 1244	0.75 1063	0.15 724	0.08 608		
H O H ₂ H ₂ O O ₂ OH	0.02339 +50021 +48452 +48452 +0.0727	0.02026 +50015 +48452 +48713 +0.0594	0.01776 +50011 +48404 +48711 +0.0493	0.01573 +50007 +48424 +48709 +0.0391	0.01434 +50007 +48426 +48709 +0.0295	0.00537 +50000 +48426 +48709 +0.0195	0.00108 +50000 +48426 +48709 +0.0095	0.00104 +50000 +48426 +48709 +0.0091	0.00021 +50000 +48426 +48709 +0.0091	0.00000 +50000 +48426 +48709 +0.0090	0.00000 +50000 +48426 +48709 +0.0090	0.00000 +50000 +48426 +48709 +0.0090	0.00000 +50000 +48426 +48709 +0.0090	0.00000 +50000 +48426 +48709 +0.0090		
$R = 0.60$, PERCENT FUEL = 17.35, O/F = 4.762																
Pressure, lb/sq in. abs Temperature, °K	150.00 3097	125.00 3036	107.14 2980	93.75 2940	86.09 2911	37.50 2630	15.00 2308	14.70 2300	7.50 2058	3.75 1812	1.50 1518	0.75 1317	0.15 924	0.08 786		
H O H ₂ H ₂ O O ₂ OH	0.04050 +50139 +38035 +55914 +0.0828	0.03714 +50113 +36152 +56932 +0.0716	0.03435 +50097 +36027 +56846 +0.0716	0.03193 +50078 +36031 +56766 +0.0716	0.03144 +50078 +36031 +56766 +0.0716	0.01688 +50079 +36032 +56766 +0.0716	0.00625 +50079 +36032 +56766 +0.0716	0.00605 +50079 +36032 +56766 +0.0716	0.00211 +50079 +36032 +56766 +0.0716	0.00051 +50079 +36032 +56766 +0.0716	0.00000 +50079 +36032 +56766 +0.0716	0.00000 +50079 +36032 +56766 +0.0716	0.00000 +50079 +36032 +56766 +0.0716	0.00000 +50079 +36032 +56766 +0.0716		
$R = 0.70$, PERCENT FUEL = 15.25, O/F = 5.556																
Pressure, lb/sq in. abs Temperature, °K	150.00 3434	125.00 3476	107.14 3420	93.75 3485	86.66 3423	37.50 3220	15.00 2990	14.70 2994	7.50 2351	3.75 2104	1.50 1747	0.75 1579	0.15 1144	0.08 983		
H O H ₂ H ₂ O O ₂ OH	0.15131 +50446 +48454 +48454 +0.0493	0.14276 +50424 +48424 +48424 +0.0493	0.13427 +50404 +48404 +48404 +0.0493	0.12479 +50384 +48384 +48384 +0.0493	0.12426 +50364 +48364 +48364 +0.0493	0.05604 +50344 +48344 +48344 +0.0493	0.01631 +50324 +48324 +48324 +0.0493	0.00561 +50324 +48324 +48324 +0.0493	0.00211 +50324 +48324 +48324 +0.0493	0.00053 +50324 +48324 +48324 +0.0493	0.00000 +50324 +48324 +48324 +0.0493	0.00000 +50324 +48324 +48324 +0.0493	0.00000 +50324 +48324 +48324 +0.0493	0.00000 +50324 +48324 +48324 +0.0493		

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute.

R = 0.80 * PERCENT FULL = 13.6L / O/F = 6.349																
Pressure, lb/sq in. abs Temperature, °K	150.00 3304	125.00 3253	107.14 3211	93.75 3174	86.97 3154	37.50 2737	15.00 2704	4.70 2694	7.50 2566	3.75 2536	1.50 2456	0.75 2064	0.15 1846	0.08 1572	0.04 1199	
H	0.05409 • 00948	0.05174 • 00870	0.04977 • 00809	0.04807 • 00752	0.04714 • 00723	0.03661 • 00431	0.02552 • 00197	0.01250 • 00193	0.01751 • 00193	0.01028 • 00084	0.00345 • 00025	0.00103 • 00000	0.00004 • 00000	0.00000 • 00000	0.00000 • 00000	
O	• 22134 • 63749	• 21952 • 64703	• 21680 • 65128	• 21669 • 65479	• 21597 • 67431	• 20826 • 74301	• 20361 • 74379	• 16049 • 66699	• 19803 • 76523	• 19761 • 76547	• 19551 • 76564	• 19951 • 79415	• 19951 • 79499	• 19951 • 79599	• 20000 • 00000	
H ₂	• 01095 • 06624	• 01030 • 06271	• 00973 • 05974	• 00925 • 05719	• 00897 • 05571	• 00593 • 04031	• 00300 • 02489	• 00294 • 04247	• 00135 • 01466	• 00041 • 00712	• 00003 • 00159	• 00000 • 00031	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	
H ₂ O																
O ₂																
OH																
R = 0.90, PERCENT FULL = 12.2+, O/F = 7.143																
Pressure, lb/sq in. abs Temperature, °K	150.00 3336	125.00 3286	107.14 3246	93.75 3211	87.09 3192	37.50 2984	15.00 2773	4.70 2770	7.50 2623	3.75 2474	1.50 2267	0.75 2092	0.15 1846	0.08 1457	0.04 1084	
H	0.05120 • 01521	0.04913 • 01428	0.04740 • 01351	0.04592 • 01287	0.04515 • 01252	0.03611 • 00882	0.02704 • 00249	0.012685 • 00543	0.02072 • 00347	0.01493 • 00190	0.00823 • 00057	0.00416 • 00013	0.00023 • 00000	0.00004 • 00000	0.00000 • 00000	
O	• 16903 • 65494	• 16643 • 65481	• 16418 • 67313	• 16222 • 66031	• 16113 • 68447	• 14905 • 72893	• 13461 • 77375	• 13450 • 7677	• 12424 • 5023	• 11474 • 40401	• 10473 • 37558	• 10075 • 89004	• 9992 • 59777	• 9992 • 89997	• 9992 • 00001	
H ₂	• 02360 • 02289	• 02226 • 02171	• 02140 • 01759	• 02140 • 06002	• 02140 • 04411	• 01300 • 01289	• 01289 • 04377	• 00936 • 03291	• 00583 • 02259	• 00205 • 01086	• 00049 • 00444	• 00004 • 00009	• 00000 • 00000	• 00000 • 00000	• 00000 • 00001	
H ₂ O																
O ₂																
OH																
R = 1.00, PERCENT FULL = 11.1+, O/F = 7.937																
Pressure, lb/sq in. abs Temperature, °K	150.00 3341	125.00 3292	107.14 3252	93.75 3211	87.13 3192	37.50 2984	15.00 2789	4.70 2787	7.50 2544	3.75 2505	1.50 2325	0.75 2188	0.15 1850	0.08 1460	0.04 1080	
H	0.04560 • 02044	0.04368 • 01940	0.04207 • 01854	0.04069 • 01781	0.03994 • 01741	0.03168 • 01317	0.02349 • 00921	0.02332 • 00913	0.01792 • 00193	0.01297 • 00213	0.00755 • 00058	0.00442 • 00123	0.00007 • 00013	0.00000 • 00003	0.00000 • 00003	
O	• 13070 • 66145	• 12778 • 67146	• 12526 • 67991	• 12306 • 68721	• 12186 • 69121	• 10759 • 73890	• 10759 • 78551	• 10759 • 8656	• 10212 • 85611	• 10162 • 85611	• 05866 • 00366					
H ₂	• 06143 • 16847	• 06080 • 16983	• 06047 • 17097	• 06000 • 17195	• 05979 • 17249	• 05862 • 17482	• 05862 • 18443	• 05862 • 18443	• 05758 • 18443	• 05758 • 18443	• 05758 • 18443	• 05758 • 18443	• 05758 • 18443	• 05758 • 00366	• 05758 • 00366	
H ₂ O	• 10038 • 16847	• 09881 • 16983	• 09840 • 17097	• 09800 • 17195	• 09772 • 17249	• 09750 • 17249	• 09750 • 17718	• 09562 • 09562	• 09515 • 09515	• 04036 • 04036	• 02661 • 02661	• 01220 • 01220	• 00248 • 00248	• 00026 • 00026	• 00000 • 00000	
O ₂																
OH																
R = 1.50, PERCENT FULL = 7.74, O/F = 1.905																
Pressure, lb/sq in. abs Temperature, °K	150.00 3219	125.00 3169	107.14 3127	93.75 3091	86.98 3071	37.50 2853	15.00 2626	4.70 2621	7.50 2455	3.75 2281	1.50 2037	0.75 1842	0.15 1393	0.08 1220	0.04 1080	
H	0.01925 • 02906	0.01792 • 02743	0.01683 • 02607	0.01591 • 02491	0.01540 • 02427	0.01017 • 01747	0.00563 • 01103	0.00554 • 01090	0.00393 • 00698	0.00309 • 00382	0.00030 • 00112	0.00000 • 00035	0.00000 • 00000	0.00000 • 00000	0.00000 • 00000	
O	• 04359 • 08666	• 04143 • 08157	• 03961 • 07730	• 03805 • 07300	• 03718 • 07280	• 02759 • 06417	• 01796 • 06411	• 01776 • 06411	• 01622 • 06411	• 01162 • 06411	• 00649 • 06411					
H ₂	• 08282 • 16847	• 08180 • 16983	• 08040 • 17097	• 08000 • 17195	• 07978 • 17249	• 07867 • 17249	• 07867 • 17718	• 07758 • 17718	• 07558 • 17718	• 07558 • 17718	• 07558 • 17718	• 07558 • 17718	• 07558 • 17718	• 07558 • 17718	• 07558 • 17718	
H ₂ O																
O ₂																
OH																
R = 2.00, PERCENT FULL = 5.92, O/F = 5.873																
Pressure, lb/sq in. abs Temperature, °K	150.00 3045	125.00 2992	107.14 2947	93.75 2909	86.67 2885	37.50 2849	15.00 2588	4.70 2584	7.50 2184	3.75 1974	1.50 1624	0.75 1492	0.15 1084	0.08 935	0.04 895	
H	0.00745 • 02225	0.00667 • 02043	0.00604 • 01983	0.00552 • 01767	0.00523 • 01694	0.00263 • 01005	0.00091 • 00453	0.00088 • 00443	0.00029 • 00194	0.00029 • 00061	0.00000 • 00007	0.00000 • 00001	0.00000 • 00000	0.00000 • 00000	0.00000 • 00000	
O	• 01742 • 01608	• 01497 • 01403	• 01403 • 01348	• 01403 • 00819	• 00379 • 00379	• 00379 • 00379	• 00379 • 00379	• 00379 • 00379	• 00371 • 00166	• 00371 • 00054	• 00007 • 00007	• 00001 • 00001	• 00000 • 00001	• 00000 • 00000	• 00000 • 00000	
H ₂	• 05708 • 29454	• 57738 • 29184	• 56203 • 29184	• 55746 • 29184	• 55746 • 29184	• 55746 • 29184	• 55746 • 29184	• 55746 • 29184	• 55746 • 29184	• 55746 • 29184	• 55746 • 29184					
H ₂ O																
O ₂																
OH																
R = 3.00, PERCENT FULL = 4.03, O/F = 3.810																
Pressure, lb/sq in. abs Temperature, °K	150.00 2695	125.00 2634	107.14 2582	93.75 2537	85.58 2507	37.50 2226	15.00 1914	4.70 1907	7.50 1687	3.75 1475	1.50 1224	0.75 1057	0.15 736	0.08 625	0.04 585	
H	0.00096 • 00762	0.00077 • 00641	0.00062 • 00549	0.00051 • 00429	0.00045 • 00224	0.00010 • 00139	0.00001 • 00023	0.00001 • 00022	0.00000 • 00004	0.00000 • 00002						
O	• 00307 • 03407	• 00260 • 03407	• 00224 • 04734	• 00195 • 47357	• 00176 • 47357	• 00059 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	• 00010 • 47357	
H ₂	• 46923 • 57335	• 46284 • 57335	• 46470 • 57335	• 46562 • 57335	• 46734 • 57335	• 46449 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	• 46466 • 57335	
H ₂ O																
O ₂																
OH																
R = 4.00, PERCENT FULL = 3.05, O/F = 1.746																
Pressure, lb/sq in. abs Temperature, °K	150.00 2363	125.00 2295	107.14 2238	93.75 2188	84.31 2149	37.50 1899	15.00 1722	4.70 1722	7.50 1520	3.75 1160	1.50 705	0.75 456	0.15 292	0.08 193	0.04 1080	
H	0.00009 • 00169	0.00006 • 00126	0.00004 • 00097	0.00003 • 00076	0.00002 • 00054	0.00000 • 00032	0.00000 • 00010	0.00000 • 00009	0.00000 • 00008	0.00000 • 00007	0.00000 • 00006	0.00000 • 00005	0.00000 • 00004	0.00000 • 00003	0.00000 • 00002	
O	• 00169 • 00169	• 00126 • 00126	• 00097 • 00097	• 00076 • 00076	• 00054 • 00054	• 00032 • 00032	• 00010 • 00010	• 00009 • 00009	• 00008 • 00008	• 00007 • 00007	• 00006 • 00006	• 00005 • 00005	• 00004 • 00004	• 00003 • 00003	• 00002 • 00002	
H ₂	• 00047 • 00047	• 00035 • 00035	• 00027 • 00027	• 00022 • 00022	• 00018 • 00018	• 00008 • 00008	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	
H ₂ O	• 00047 • 00047	• 00035 • 00035	• 00027 • 00027	• 00022 • 00022	• 00018 • 00018	• 00008 • 00008	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	• 00000 • 00000	
O ₂			</td													

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Combustion-chamber pressure, 300 pounds per square inch absolute

R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190															
Pressure, lb/sq in. abs Temperature, °K	300.00 1183	250.00 1129	214.29 1085	187.50 1049	160.84 1008	75.00 624	30.00 643	15.00 532	14.70 529	7.50 439	3.00 340	1.50 280	0.30 175	0.15 142	
H ₂ H ₂ O	0.85000 •15000														
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587															
Pressure, lb/sq in. abs Temperature, °K	300.00 1514	250.00 1450	214.29 1398	187.50 1354	162.47 1307	75.00 1079	30.00 852	15.00 709	14.70 705	7.50 588	3.00 458	1.50 379	0.30 242	0.15 198	
H ₂ H ₂ O	0.80000 •20000														
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984															
Pressure, lb/sq in. abs Temperature, °K	300.00 1817	250.00 1745	214.29 1663	187.50 1636	165.91 1587	75.00 1322	30.00 1157	15.00 887	14.70 882	7.50 741	3.00 581	1.50 482	0.30 310	0.15 256	
H H ₂ H ₂ O	0.00000 •74993 •24999	0.00000 •74996 •24999	0.00000 •74997 •25000	0.00000 •74998 •25000	0.00000 •74999 •25000	0.00000 •75000 •25000	0.00000 •75000 •25000								
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381															
Pressure, lb/sq in. abs Temperature, °K	300.00 2093	250.00 2016	214.29 1952	187.50 1897	165.12 1846	75.00 1553	30.00 1257	15.00 1084	14.70 1059	7.50 895	3.00 707	1.50 590	0.30 383	0.15 317	
H H ₂ H ₂ O OH	0.00055 •69954 •29988 •00003	0.00037 •69969 •29993 •00002	0.00025 •69979 •29995 •00001	0.00018 •69985 •29997 •00001	0.00013 •69988 •29998 •00000	0.00001 •69999 •30000 •00000	0.00000 •70000 •30000 •00000								
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778															
Pressure, lb/sq in. abs Temperature, °K	300.00 2344	250.00 2263	214.29 2196	187.50 2139	166.26 2088	75.00 1771	30.00 1451	15.00 1238	14.70 1232	7.50 1051	3.00 838	1.50 702	0.30 460	0.15 362	
H H ₂ H ₂ O OH	0.00214 •64827 •34939 •00020	0.00155 •64875 •34957 •00013	0.00116 •64906 •34999 •00009	0.00089 •64928 •34979 •00006	0.00069 •64992 •34983 •00004	0.00010 •65000 •35000 •00000	0.00001 •65000 •35000 •00000	0.00000 •65000 •35000 •00000							
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175															
Pressure, lb/sq in. abs Temperature, °K	300.00 2565	250.00 2484	214.29 2417	187.50 2359	167.44 2310	75.00 1978	30.00 1637	15.00 1409	14.70 1403	7.50 1205	3.00 970	1.50 819	0.30 542	0.15 452	
H O H ₂ H ₂ O OH	0.00565 •59566 •39782 •00086	0.00437 •59562 •39839 •00061	0.00347 •59571 •39839 •00045	0.00281 •59782 •39877 •00034	0.00233 •59918 •39903 •00026	0.00048 •59962 •39987 •00026	0.00004 •59997 •39998 •00003	0.00000 •60000 •40000 •00000							
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571															
Pressure, lb/sq in. abs Temperature, °K	300.00 2755	250.00 2677	214.29 2611	187.50 2555	168.67 2510	75.00 2173	30.00 1818	15.00 1576	14.70 1569	7.50 1358	3.00 1105	1.50 938	0.30 630	0.15 527	
H O H ₂ H ₂ O O ₂ OH	0.01130 •00003 •54185 •16423 •00001 •00258	0.00527 •00002 •54328 •44547 •00001 •00196	0.00773 •00001 •54436 •44702 •00000 •00153	0.00654 •00001 •54521 •44747 •00000 •00122	0.00570 •00001 •54582 •44743 •00000 •00101	0.00570 •00001 •54582 •44743 •00000 •00118	0.00157 •00001 •54582 •44743 •00000 •00001	0.00003 •00000 •54582 •44743 •00000 •00001	0.00000 •00000 •54582 •44743 •00000 •00000	0.00000 •00000 •54582 •44743 •00000 •00000	0.00000 •00000 •54582 •44743 •00000 •00000	0.00000 •00000 •54582 •44743 •00000 •00000	0.00000 •00000 •54582 •44743 •00000 •00000	0.00000 •00000 •54582 •44743 •00000 •00000	
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968															
Pressure, lb/sq in. abs Temperature, °K	300.00 2915	250.00 2841	214.29 2778	187.50 2724	169.85 2684	75.00 2352	30.00 1992	15.00 1740	14.70 1732	7.50 1509	3.00 1240	1.50 1060	0.30 722	0.15 607	
H O H ₂ H ₂ O O ₂ OH	0.01858 •00014 •48771 •48758 •00006 •00595	0.01592 •00010 •49336 •49177 •00004 •00479	0.01383 •00007 •49253 •49275 •00003 •00328	0.01214 •00005 •49253 •49275 •00002 •00285	0.01097 •00004 •49252 •49274 •00001 •00070	0.00391 •00000 •49252 •49274 •00000 •00008	0.00015 •00000 •49252 •49274 •00000 •00001	0.00014 •00000 •49252 •49274 •00000 •00001	0.00002 •00000 •49252 •49274 •00000 •00001	0.00000 •00000 •49252 •49274 •00000 •00001	0.00000 •00000 •49252 •49274 •00000 •00001	0.00000 •00000 •49252 •49274 •00000 •00001	0.00000 •00000 •49252 •49274 •00000 •00001		
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762															
Pressure, lb/sq in. abs Temperature, °K	300.00 3155	250.00 3089	214.29 3033	187.50 2985	171.73 2953	75.00 2652	30.00 2511	15.00 2024	14.70 2047	7.50 1808	3.00 1512	1.50 1311	0.30 919	0.15 782	
H O H ₂ H ₂ O O ₂ OH	0.03386 •00100 •56191 •00059 •01907	0.03080 •00080 •56664 •00047 •01664	0.02826 •00065 •57038 •00044 •01470	0.02611 •00054 •57341 •00037 •01313	0.02472 •00047 •57341 •00027 •01214	0.01303 •00040 •57341 •00026 •01214	0.00450 •00040 •57341 •00026 •01214	0.00145 •00040 •57341 •00026 •01214	0.00140 •00040 •57341 •00026 •01214	0.00034 •00034 •57341 •00026 •01214	0.00003 •00003 •57341 •00026 •01214	0.00000 •00000 •57341 •00026 •01214	0.00000 •00000 •57341 •00026 •01214		
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556															
Pressure, lb/sq in. abs Temperature, °K	300.00 3307	250.00 3245	214.29 3190	187.50 3152	172.98 3120	75.00 2655	30.00 2569	15.00 2355	14.70 2328	7.50 2079	3.00 1765	1.50 1566	0.30 1133	0.15 975	
H O H ₂ H ₂ O O ₂ OH	0.14433 •00168 •49340 •00233 •02222 •02222	0.09500 •00245 •49340 •00233 •02222 •02222	0.08260 •00233 •49340 •00233 •02222 •02222	0.07240 •00223 •49340 •00233 •02222 •02222	0.06240 •00213 •49340 •00233 •02222 •02222	0.01780 •00178 •49340 •00233 •02222 •02222	0.00623 •00623 •49340 •00233 •02222 •02222	0.00623 •00623 •49340 •00233 •02222 •02222	0.00623 •00623 •49340 •00233 •02222 •02222	0.00230 •00230 •49340 •00233 •02222 •02222	0.00038 •00038 •49340 •00233 •02222 •02222	0.00007 •00007 •49340 •00233 •02222 •02222	0.00000 •00000 •49340 •00233 •02222 •02222		

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute

R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349														
Pressure, lb/sq in. abs Temperature, °K	300.00 3393	250.00 333d	214.29 3292	187.50 3253	173.68 3231	75.00 2999	30.00 2744	15.00 2599	14.70 2544	7.50 2544	3.00 2403	1.50 1610	O/F 1360	O/F 1165
H	0.04749	0.04529	0.04344	0.04185	0.04094	0.03116	0.02091	0.01370	0.01349	0.00724	0.00428	0.00064	0.00001	0.00000
O	+0.0793	+0.0772	+0.0665	+0.0617	+0.0590	+0.0334	+0.0193	+0.0053	+0.0051	+0.0013	+0.0001	+0.0000	+0.0000	+0.0000
H ₂	+2.002	+2.1819	+2.1667	+2.1556	+2.1463	+2.0716	+2.0102	+1.9624	+1.9524	+1.9867	+2.0000	+1.9967	+2.0000	+2.0000
H ₂ O	+65200	+66098	+66494	+67492	+67826	+71664	+72626	+77424	+77482	+76873	+79759	+79946	+80000	+80000
O ₂	+0.0939	+0.0876	+0.0827	+0.0776	+0.0759	+0.0470	+0.0215	+0.0086	+0.0083	+0.0022	+0.0001	+0.0000	+0.0000	+0.0000
OH	+0.6318	+0.5956	+0.5655	+0.5393	+0.5245	+0.3681	+0.2124	+0.1434	+0.1180	+0.0247	+0.0103	+0.0019	+0.0000	+0.0000
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143														
Pressure, lb/sq in. abs Temperature, °K	300.00 3430	250.00 3377	214.29 3334	187.50 3298	173.68 3276	75.00 3054	30.00 2829	15.00 2666	14.70 2601	7.50 2503	3.00 2476	1.50 2084	O/F 1600	O/F 1416
H	0.04506	0.04313	0.04153	0.04015	0.03939	0.03109	0.02478	0.01705	0.01689	0.01187	0.00005	0.00278	0.00013	0.00002
O	+0.1323	+0.1237	+0.1167	+0.1107	+0.1075	+0.0674	+0.04734	+0.0259	+0.0259	+0.0133	+0.0033	+0.0006	+0.0000	+0.0000
H ₂	+16552	+16261	+16051	+15890	+15757	+14464	+14029	+14201	+14147	+14266	+14027	+0.9992	+0.9999	+0.9999
H ₂ O	+67094	+66077	+66904	+66919	+70016	+74431	+79034	+82111	+82352	+85109	+88117	+89314	+89887	+89999
O ₂	+0.02140	+0.02068	+0.02006	+0.01950	+0.01919	+0.01540	+0.01090	+0.0045	+0.00735	+0.00423	+0.0119	+0.00422	+0.0000	+0.0000
OH	+0.8385	+0.8023	+0.7720	+0.7458	+0.7313	+0.5721	+0.4098	+0.2566	+0.2934	+0.1940	+0.00249	+0.00295	+0.0005	+0.0000
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937														
Pressure, lb/sq in. abs Temperature, °K	300.00 3437	250.00 3384	214.29 3341	187.50 3284	174.06 3205	75.00 2647	30.00 2472	15.00 2292	14.70 2087	7.50 2044	3.00 2003	1.50 1839	O/F 1608	O/F 1415
H	0.03987	0.03809	0.03661	0.03534	0.03464	0.02707	0.01963	0.0167	0.01421	0.01030	0.00569	0.00313	0.00032	0.00006
O	+0.1816	+0.1719	+0.1639	+0.1571	+0.1534	+0.1143	+0.0782	+0.0255	+0.0254	+0.0166	+0.0095	+0.0007	+0.0001	+0.0000
H ₂	+12585	+12283	+12029	+11800	+11674	+10213	+08626	+0783	+07444	+05591	+04302	+03088	+00874	+00356
H ₂ O	+67806	+66805	+65646	+65646	+70377	+70783	+75526	+80148	+8367	+85769	+87144	+89446	+93392	+93392
O ₂	+0.03906	+0.03851	+0.03802	+0.03758	+0.03733	+0.03412	+0.02949	+0.0230	+0.02618	+0.02332	+0.01667	+0.01232	+0.00313	+0.0017
OH	+0.09900	+0.09532	+0.09224	+0.08959	+0.08613	+0.07197	+0.05551	+0.0401	+0.04369	+0.0348	+0.02124	+0.01574	+0.00470	+0.00067
R = 1.50, PERCENT FUEL = 7.749, O/F = 1.905														
Pressure, lb/sq in. abs Temperature, °K	300.00 3297	250.00 3243	214.29 3198	187.50 3159	173.72 3137	75.00 2904	30.00 2661	15.00 2478	14.70 2472	7.50 2291	3.00 2032	1.50 1830	O/F 1607	O/F 1407
H	0.01582	0.01466	0.01370	0.01289	0.01243	0.00798	0.00516	0.0016	0.00211	0.00090	0.00017	0.00003	0.00000	0.00000
O	+0.02582	+0.02428	+0.02300	+0.02192	+0.02131	+0.01498	+0.00911	+0.0054	+0.00544	+0.00287	+0.00043	+0.00244	+0.0000	+0.0000
H ₂	+0.3926	+0.3716	+0.3540	+0.3388	+0.3302	+0.2388	+0.1929	+0.1200	+0.1116	+0.0800	+0.0468	+0.0145	+0.0040	+0.0000
H ₂ O	+64080	+64897	+65520	+66166	+66449	+70013	+73545	+75581	+75741	+77472	+79041	+79584	+79980	+79980
O ₂	+0.16901	+0.17040	+0.17157	+0.17257	+0.17313	+0.17919	+0.18235	+0.18794	+0.18971	+0.19335	+0.19708	+0.19870	+0.19994	+0.19994
OH	+0.10299	+0.10454	+0.10054	+0.09708	+0.09512	+0.07367	+0.05198	+0.0366	+0.03623	+0.03231	+0.01400	+0.00415	+0.00019	+0.00003
R = 2.00, PERCENT FUEL = 5.927, O/F = 5.873														
Pressure, lb/sq in. abs Temperature, °K	300.00 3103	250.00 3046	214.29 2998	187.50 2957	173.03 2932	75.00 2679	30.00 2402	15.00 2188	14.70 2181	7.50 2170	3.00 1666	1.50 1483	O/F 1076	O/F 0929
H	0.00578	0.00513	0.00461	0.00419	0.00395	0.00148	0.00060	0.00318	0.00017	0.00000	0.00000	0.00000	0.00000	0.00000
O	+0.1907	+0.1742	+0.1603	+0.1491	+0.1424	+0.0813	+0.0346	+0.0140	+0.0136	+0.00402	+0.0005	+0.0001	+0.0000	+0.0000
H ₂	+11498	+10375	+0.1273	+0.1187	+0.1136	+0.0564	+0.0289	+0.0120	+0.0116	+0.00307	+0.0004	+0.0001	+0.0000	+0.0000
H ₂ O	+57933	+56564	+59085	+59085	+59788	+62279	+64414	+6524	+65520	+66111	+66562	+66642	+66666	+66667
O ₂	+29800	+30043	+30244	+30414	+30212	+25354	+24141	+24042	+24113	+22833	+33344	+33333	+33333	+33333
OH	+0.08282	+0.07765	+0.07333	+0.06963	+0.06742	+0.04564	+0.02336	+0.01377	+0.01348	+0.00614	+0.00145	+0.00036	+0.0000	+0.0000
R = 3.00, PERCENT FUEL = 4.031, O/F = 3.810														
Pressure, lb/sq in. abs Temperature, °K	300.00 2723	250.00 2658	214.29 2604	187.50 2523	170.82 2232	75.00 1914	30.00 1584	15.00 1184	14.70 1178	7.50 1072	3.00 1222	1.50 1055	O/F 735	O/F 623
H	0.00067	0.00053	0.00042	0.00035	0.00030	0.00006	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
O	+0.00605	+0.00505	+0.00428	+0.00368	+0.00330	+0.00102	+0.0016	+0.0003	+0.0002	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000
H ₂	+0.0244	+0.0205	+0.0175	+0.0151	+0.0136	+0.00403	+0.0007	+0.0001	+0.0001	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000
H ₂ O	+47287	+47630	+47900	+48120	+48265	+49253	+49742	+49740	+49742	+49947	+49947	+49947	+50000	+50000
O ₂	+48280	+48501	+48675	+48616	+48609	+49537	+49537	+49537	+49537	+49964	+49964	+49964	+50000	+50000
OH	+0.03516	+0.03107	+0.02779	+0.02510	+0.02330	+0.01058	+0.00312	+0.0093	+0.00889	+0.00021	+0.00002	+0.00000	+0.00000	+0.00000
R = 4.00, PERCENT FUEL = 3.054, O/F = 1.746														
Pressure, lb/sq in. abs Temperature, °K	300.00 2372	250.00 2303	214.29 2244	187.50 2194	168.42 2153	75.00 1659	30.00 1555	15.00 1349	14.70 1343	7.50 1183	3.00 1121	1.50 0724	O/F 0403	O/F 0403
H	0.00006	0.00000	0.00003	0.00002	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
O	+0.0126	+0.0094	+0.0071	+0.0056	+0.0045	+0.0007	+0.0000	+0.0000	+0.0000	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000
H ₂	+0.00325	+0.0026	+0.0020	+0.0016	+0.0013	+0.0002	+0.0000	+0.0000	+0.0000	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000
H ₂ O	+39225	+39372	+39480	+39562	+39621	+39893	+39883	+39877	+39877	+39947	+40000	+40000	+40000	+40000
O ₂	+59436	+59547	+59627	+59687	+59720	+59925	+59925	+59925	+59925	+60000	+60000	+60000	+60000	+60000
OH	+0.01171	+0.00958	+0.00799	+0.00677	+0.00589	+0.00172	+0.00025	+0.00025	+0.00025	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000
R = 5.00, PERCENT FUEL = 2.458, O/F = 9.683														
Pressure, lb/sq in. abs Temperature, °K	300.00 2069	250.00 2000	214.29 1947	187.50 1893	165.43 1821	75.00 1578	30.00 1503	15.00 1349	14.70 1343	7.50 1183	3.00 1121	1.50 0724	O/F 0403	O/F 0403
H	0.00020	0.00013	0.00009	0.00006	0.00005	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
O	+0.0004	+0.0002	+0.00007	+0.00001	+0.00001	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000	+0.00000
H ₂	+33131	+33182</td												

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Combustion-chamber pressure, 600 pounds per square inch absolute

R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190																
Pressure, lb/sq in. abs Temperature, °K	600.00 1183	500.00 1129	428.57 1049	375.00 1049	321.68 1008	150.00 824	60.00 643	30.00 534	15.00 439	14.70 437	6.00 340	3.00 280	0.60 175	0.30 142		
H ₂ H ₂ O	0.85000 +15000															
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587																
Pressure, lb/sq in. abs Temperature, °K	600.00 1514	500.00 1450	428.57 1398	375.00 1354	324.94 1307	150.00 1079	60.00 852	30.00 709	15.00 588	14.70 585	6.00 458	3.00 379	0.60 242	0.30 198		
H ₂ H ₂ O	0.80000 +20000															
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984																
Pressure, lb/sq in. abs Temperature, °K	600.00 1817	500.00 1745	428.57 1686	375.00 1636	327.81 1567	150.00 1322	60.00 1057	30.00 887	15.00 741	14.70 737	6.00 581	3.00 482	0.60 310	0.30 256		
H H ₂ H ₂ O	0.0006 +74995 +24999	0.00003 +74997 +25000	0.00002 +74998 +25000	0.00001 +74999 +25000	0.00001 +75000 +25000	0.00000 +75000 +25000										
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381																
Pressure, lb/sq in. abs Temperature, °K	600.00 2094	500.00 2016	428.57 1952	375.00 1898	330.21 1847	150.00 1553	60.00 1257	30.00 1064	15.00 895	14.70 891	6.00 707	3.00 590	0.60 383	0.30 317		
H H ₂ H ₂ O OH	0.00019 +69967 +29992 +00002	0.00026 +69978 +29995 +00001	0.00018 +69985 +29996 +00000	0.00013 +69988 +29998 +00000	0.00009 +69992 +29998 +00000	0.00001 +69999 +29998 +00000	0.00000 +70000 +30000 +00000									
R = 0.35, PERCENT FUEL = 26.47*, O/F = 2.778																
Pressure, lb/sq in. abs Temperature, °K	600.00 2347	500.00 2266	428.57 2199	375.00 2089	332.36 2089	150.00 1771	60.00 1451	30.00 1238	15.00 1050	14.70 1045	6.00 838	3.00 702	0.60 460	0.30 382		
H H ₂ H ₂ O OH	0.00154 +64875 +34956 +00015	0.00111 +64910 +34969 +00009	0.00033 +64933 +34978 +00005	0.00063 +64944 +34984 +00004	0.00049 +64949 +34988 +00003	0.00007 +64994 +34998 +00000	0.00000 +65000 +35000 +00000									
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175																
Pressure, lb/sq in. abs Temperature, °K	600.00 2574	500.00 2492	428.57 2422	375.00 2363	334.53 2312	150.00 1978	60.00 1637	30.00 1408	15.00 1204	14.70 1199	6.00 970	3.00 818	0.60 542	0.30 452		
H H ₂ H ₂ O OH	0.00016 +59681 +39339 +00045	0.00020 +59753 +39882 +00045	0.00020 +59805 +39910 +00005	0.00023 +59842 +39930 +00004	0.00017 +59870 +39930 +00003	0.00034 +59973 +39991 +00001	0.00003 +59998 +39991 +00000	0.00000 +60000 +40000 +00000								
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571																
Pressure, lb/sq in. abs Temperature, °K	600.00 2773	500.00 2692	428.57 2624	375.00 2563	336.53 2312	150.00 1978	60.00 1637	30.00 1408	15.00 1204	14.70 1199	6.00 970	3.00 818	0.60 542	0.30 452		
H O H ₂ H ₂ O O ₂ OH	0.00016 +59685 +34383 +44560 +00001 +00198	0.00020 +59753 +34545 +44659 +00000 +00149	0.00017 +59805 +34546 +44728 +00000 +00115	0.00020 +59842 +34546 +44779 +00000 +00074	0.00017 +59870 +34546 +44779 +00000 +00013	0.00012 +59973 +34546 +44959 +00000 +00001	0.00015 +59998 +34546 +44999 +00000 +00000	0.00000 +60000 +40000 +00000 +00000								
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968																
Pressure, lb/sq in. abs Temperature, °K	600.00 2944	500.00 2866	428.57 2800	375.00 2762	338.88 2699	150.00 2356	60.00 1990	30.00 1737	15.00 1507	14.70 1501	6.00 1238	3.00 1059	0.60 720	0.30 606		
H O H ₂ H ₂ O O ₂ OH	0.01447 +59609 +49042 +49024 +00003 +00475	0.01228 +59753 +49190 +49127 +00002 +00377	0.01057 +59805 +49208 +49207 +00002 +00307	0.00921 +59842 +49208 +49207 +00001 +00253	0.00825 +59973 +49208 +49207 +00001 +00218	0.00828 +59998 +49208 +49207 +00000 +00050	0.00053 +59998 +49208 +49207 +00000 +00005	0.00010 +59998 +49208 +49207 +00000 +00001	C.00001 +59998 +49208 +49207 +00000 +00001	C.00001 +59998 +49208 +49207 +00000 +00001	C.00001 +59998 +49208 +49207 +00000 +00001	0.00000 +59998 +49208 +49207 +00000 +00001	0.00000 +59998 +49208 +49207 +00000 +00001	0.00000 +59998 +49208 +49207 +00000 +00001	0.00000 +59998 +49208 +49207 +00000 +00001	0.00000 +59998 +49208 +49207 +00000 +00001
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762																
Pressure, lb/sq in. abs Temperature, °K	600.00 3208	500.00 3137	428.57 3025	375.00 2990	342.61 2990	150.00 2313	60.00 2020	30.00 1803	15.00 1603	14.70 1796	6.00 1506	3.00 1306	0.60 916	0.30 778		
H O H ₂ H ₂ O O ₂ OH	0.32778 +30669 +36551 +36551 +00041 +01629	0.32066 +30554 +36851 +36851 +00037 +01466	0.32282 +30404 +36851 +36851 +00026 +01466	0.31970 +30315 +36940 +36940 +00020 +01466	0.31988 +30315 +36940 +36940 +00019 +01466	0.31988 +30315 +36940 +36940 +00018 +01466	0.00321 +30315 +36940 +36940 +00018 +01466	0.00100 +30315 +36940 +36940 +00018 +01466	0.00023 +30315 +36940 +36940 +00018 +01466	0.00023 +30315 +36940 +36940 +00018 +01466	0.00023 +30315 +36940 +36940 +00018 +01466	0.00000 +30315 +36940 +36940 +00018 +01466	0.00000 +30315 +36940 +36940 +00018 +01466	0.00000 +30315 +36940 +36940 +00018 +01466	0.00000 +30315 +36940 +36940 +00018 +01466	
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556																
Pressure, lb/sq in. abs Temperature, °K	600.00 3381	500.00 3317	428.57 3265	375.00 3217	345.24 3168	150.00 2903	60.00 2264	30.00 2337	15.00 2086	14.70 2081	6.00 1775	3.00 1556	0.60 1129	0.30 966		
H O H ₂ H ₂ O O ₂ OH	0.33771 +30269 +36362 +36362 +00041 +01629	0.33146 +30249 +36352 +36352 +00037 +01466	0.33136 +30249 +36352 +36352 +00037 +01466	0.33126 +30249 +36352 +36352 +00037 +01466	0.33126 +30249 +36352 +36352 +00037 +01466	0.33126 +30249 +36352 +36352 +00037 +01466	0.01959 +30249 +36352 +36352 +00037 +01466	0.00964 +30249 +36352 +36352 +00037 +01466	0.00442 +30249 +36352 +36352 +00037 +01466	0.00442 +30249 +36352 +36352 +00037 +01466	0.00442 +30249 +36352 +36352 +00037 +01466	0.00025 +30249 +36352 +36352 +00037 +01466	0.00025 +30249 +36352 +36352 +00037 +01466	0.00025 +30249 +36352 +36352 +00037 +01466	0.00025 +30249 +36352 +36352 +00037 +01466	

TABLE IV. - Concluded. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute

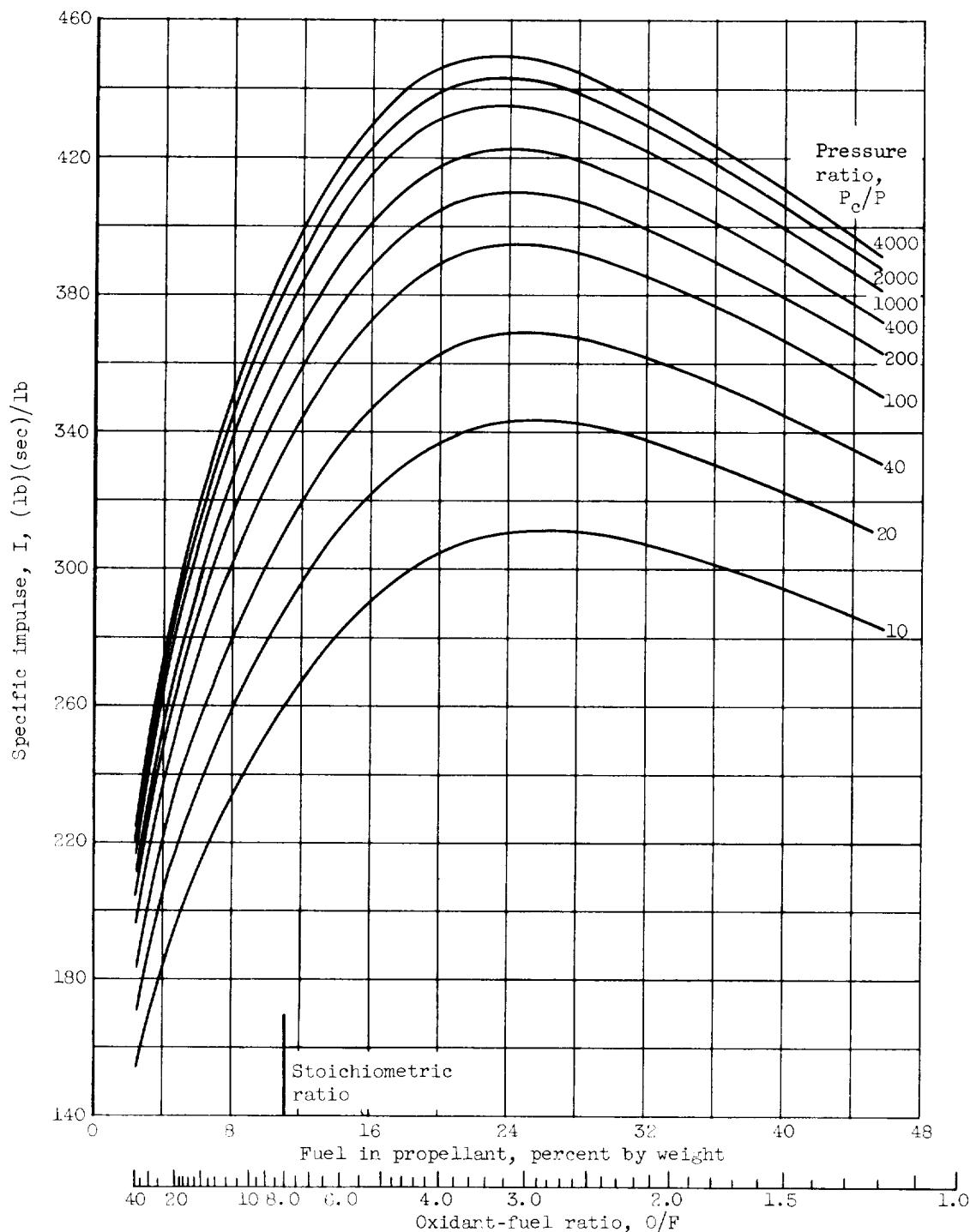
R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349																
Pressure, lb/sq in. abs Temperature, °K	600.00 3481	500.00 3422	428.57 3373	375.00 3331	346.81 3306	150.00 3092	60.00 2779	3.00 568	15.00 2346	14.70 2340	6.00 2042	3.00 1815	0.60 1347	0.30 1173		
H	0.04117	0.03913	0.03742	0.03595	0.03510	0.02609	0.01678	0.0045	0.00538	0.00526	0.00149	0.00040	0.00001	0.00000		
O	0.00646	0.00584	0.00534	0.00492	0.00468	0.00250	0.00094	0.0032	0.00007	0.00006	0.00000	0.00000	0.00000	0.00000		
H ₂	0.21839	0.21659	0.21509	0.21361	0.21308	0.20598	0.20057	0.1869	0.19855	0.19856	0.19930	0.19981	0.20000	0.20000		
H ₂ O	0.66670	0.67542	0.68269	0.68950	0.69250	0.72890	0.76212	0.7057	0.79211	0.79233	0.79845	0.79985	0.80000	0.80000		
O ₂	0.0786	0.0727	0.0678	0.0635	0.0610	0.0359	0.0147	0.0052	0.00111	0.00011	0.00000	0.00000	0.00000	0.00000		
OH	0.05941	0.05575	0.05269	0.05006	0.04854	0.03294	0.01813	0.0045	0.00378	0.00366	0.00056	0.00011	0.00000	0.00000		
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143																
Pressure, lb/sq in. abs Temperature, °K	600.00 3526	500.00 3469	428.57 3422	375.00 3382	347.52 3360	150.00 3122	60.00 2881	3.00 705	15.00 2528	14.70 2523	6.00 2279	3.00 2072	0.60 1585	0.30 1397		
H	0.03919	0.03743	0.03596	0.03469	0.03398	0.02643	0.01890	0.0378	0.00923	0.00910	0.00431	0.00182	0.00007	0.00001		
O	0.01130	0.01053	0.00989	0.00935	0.00905	0.00504	0.00250	0.0193	0.00086	0.00086	0.00017	0.00002	0.00000	0.00000		
H ₂	0.16146	0.15871	0.15636	0.15433	0.15136	0.14025	0.12644	0.1674	0.10852	0.10831	0.10171	0.10002	0.09997	0.10000		
H ₂ O	0.68792	0.69763	0.70580	0.71285	0.71686	0.76023	0.80490	0.8571	0.86232	0.86302	0.88712	0.89611	0.89993	0.89999		
O ₂	0.01917	0.01845	0.01782	0.01727	0.01695	0.01322	0.00890	0.0570	0.00292	0.00285	0.00664	0.00009	0.00000	0.00000		
OH	0.08096	0.07727	0.07417	0.07150	0.06999	0.05383	0.03743	0.0614	0.01587	0.00605	0.00190	0.00003	0.00000	0.00000		
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937																
Pressure, lb/sq in. abs Temperature, °K	600.00 3534	500.00 3478	428.57 3431	375.00 3392	347.72 3370	150.00 3137	60.00 2903	3.00 758	15.00 2578	14.70 2573	6.00 2371	3.00 2214	0.60 1866	0.30 1648		
H	0.03443	0.03281	0.03146	0.03030	0.02966	0.02281	0.01615	0.0177	0.00802	0.00792	0.00417	0.00216	0.00018	0.00003		
O	0.1593	0.1504	0.1430	0.1368	0.1334	0.0978	0.0653	0.452	0.0291	0.0286	0.0138	0.0066	0.0004	0.0001		
H ₂	0.12040	0.11731	0.11467	0.11237	0.11107	0.09622	0.07953	0.669	0.05387	0.05349	0.03741	0.02951	0.00541	0.02494		
H ₂ O	0.69574	0.70566	0.71402	0.72125	0.72534	0.7027	0.8177	0.216	0.84474	0.84567	0.94942	0.94942	0.98868	0.99587		
O ₂	0.03662	0.03605	0.03555	0.03510	0.03484	0.03159	0.02737	0.375	0.01983	0.01971	0.01437	0.01027	0.00274	0.00108		
OH	0.09689	0.09314	0.08999	0.08729	0.08577	0.06934	0.05267	0.111	0.03063	0.03034	0.01817	0.01159	0.00195	0.00058		
R = 1.50, PERCENT FUEL = 7.749, O/F = 1.905																
Pressure, lb/sq in. abs Temperature, °K	600.00 3374	500.00 3315	428.57 3267	375.00 3226	346.93 3202	150.00 2953	60.00 2692	3.00 496	15.00 2297	14.70 2291	6.00 2026	3.00 1818	0.60 1366	0.30 1195		
H	0.01276	0.01175	0.01093	0.01023	0.00984	0.00606	0.00299	0.0146	0.00056	0.00055	0.00009	0.00001	0.00000	0.00000		
O	0.02263	0.02121	0.02020	0.01902	0.01844	0.01265	0.00739	0.0430	0.0211	0.02026	0.0056	0.0004	0.0000	0.00000		
H ₂	0.03486	0.03285	0.03117	0.02972	0.02889	0.02032	0.01216	0.0720	0.0359	0.0351	0.0098	0.0025	0.00000	0.00000		
H ₂ O	0.65376	0.66167	0.66229	0.67395	0.67722	0.71084	0.74322	0.7358	0.77939	0.77979	0.79254	0.79729	0.79990	0.79998		
O ₂	0.16978	0.17119	0.17238	0.17340	0.17399	0.18014	0.18637	0.1058	0.19418	0.19427	0.19760	0.19904	0.19996	0.19999		
OH	0.10621	0.10133	0.09722	0.09368	0.09163	0.06998	0.04787	0.287	0.0216	0.01983	0.00823	0.00326	0.00014	0.00002		
R = 2.00, PERCENT FUEL = 5.927, O/F = 5.873																
Pressure, lb/sq in. abs Temperature, °K	600.00 3158	500.00 3097	428.57 3046	375.00 3002	345.45 2975	150.00 2706	60.00 2413	3.00 189	15.00 1965	14.70 1959	6.00 1678	3.00 1475	0.60 1070	0.30 923		
H	0.00439	0.00387	0.00345	0.00311	0.00291	0.00132	0.00039	0.00111	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000		
O	0.01610	0.01611	0.01339	0.01238	0.01178	0.00648	0.00260	0.101	0.0029	0.0028	0.0003	0.0000	0.00000	0.00000		
H ₂	0.1269	0.1157	0.1065	0.09988	0.09942	0.0529	0.0218	0.086	0.0025	0.0025	0.0003	0.0000	0.00000	0.00000		
H ₂ O	0.58773	0.59871	0.59864	0.60281	0.60532	0.62843	0.64767	0.6728	0.66285	0.66296	0.66584	0.66647	0.66666	0.66667		
O ₂	0.30070	0.30305	0.30500	0.30665	0.30765	0.31693	0.32491	0.3905	0.33154	0.33151	0.33293	0.33324	0.33333	0.33333		
OH	0.07838	0.07319	0.06887	0.06517	0.06293	0.04155	0.02225	0.169	0.00505	0.00491	0.00116	0.00028	0.00000	0.00000		
R = 3.00, PERCENT FUEL = 4.031, O/F = 3.810																
Pressure, lb/sq in. abs Temperature, °K	600.00 2747	500.00 2679	428.57 2624	375.00 2573	340.99 2538	150.00 2237	60.00 1913	3.00 682	15.00 1470	14.70 1464	6.00 1220	3.00 1053	0.60 733	0.30 622		
H	0.00046	0.00036	0.00028	0.00023	0.00020	0.00004	0.00000	0.0000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000		
O	0.00474	0.00392	0.00330	0.00282	0.00251	0.00075	0.00012	0.0002	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000		
H ₂	0.00191	0.00159	0.00135	0.00116	0.00103	0.00032	0.00005	0.0001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000		
H ₂ O	0.47624	0.47934	0.4818	0.48375	0.48507	0.49370	0.49827	0.5195	0.49983	0.49990	0.49999	0.50000	0.50000	0.50000		
O ₂	0.48500	0.48699	0.48855	0.48981	0.49065	0.49611	0.49895	0.51970	0.49993	0.49999	0.49999	0.50000	0.50000	0.50000		
OH	0.03164	0.02780	0.02474	0.02244	0.02055	0.00969	0.00261	0.077	0.00017	0.00016	0.00001	0.00000	0.00000	0.00000		
R = 4.00, PERCENT FUEL = 3.054, O/F = 1.746																
Pressure, lb/sq in. abs Temperature, °K	600.00 2381	500.00 2309	428.57 2249	375.00 2198	336.49 2157	150.00 1860	60.00 1554	3.00 348	15.00 1164	14.70 1159	6.00 813	3.00 551	0.60 463	0.30 360		
H	0.00004	0.00002	0.00002	0.00001	0.00001	0.00000	0.00000	0.0000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000		
O	0.00094	0.00069	0.00052	0.00040	0.00033	0.00005	0.00000	0.0000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000		
H ₂	0.00026	0.00019	0.00015	0.00011	0.00009	0.00001	0.00000	0.0000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000		
H ₂ O	0.39338	0.39465	0.39559	0.39629	0.39680	0.39910	0.39966	0.41998	0.40000	0.40000	0.40000	0.40000	0.40000	0.40000		
O ₂	0.59523	0.59618	0.59665	0.59738	0.59774	0.59938	0.59991	0.61998	0.60000	0.60000	0.60000	0.60000	0.60000	0.60000		</td

TABLE V. - SUMMARY OF COMBUSTION PARAMETERS, CHARACTERISTIC VELOCITY, AND PERFORMANCE FOR EXPANSION TO SEA LEVEL FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

Equiv- alence ratio, R , $2(0)/H$	Fuel percent by weight	Oxidant- fuel weight ratio, O/F	Com- bus- tion tem- pera- ture, T_c , °K	Exit tem- pera- ture, T_e , °K	Charac- teristic veloc- ity, c, ft/sec	Charac- teristic- velocity exponent, n_c *	Entropy, s, cal (g)/(°K)	Area ratio, ϵ	Coeffi- cient of thrust, C_F	Specific impulse, I, (lb)/(sec)	Specific impulse, I _b
CHAMBER PRESSURE, 60 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION											
0.150	45.65	1.190	1183	819	1247	0.0000	9.3807	1.4244	1.038	233.7	
•200	38.65	1.587	1514	1073	7607	•0000	6.0172	1.2956	1.035	244.7	
•250	33.51	1.984	1616	1316	7814	•0000	7.6147	1.286	1.033	250.8	
•300	29.57	2.381	2081	1546	7930	•0000	1.4390	1.2718	1.031	254.1	
•350	26.47	2.778	2324	1764	7988	•0001	6.7611	1.289	1.029	255.4	
•400	23.45	3.175	2551	1970	•0001	•0009	6.3590	1.302	1.027	255.3	
•450	21.87	3.571	2696	2159	7973	•0025	6.0167	1.3136	1.025	254.0	
•500	20.12	3.968	2628	2361	7912	•0045	7.0722	1.3331	1.024	251.8	
•600	17.35	4.762	3015	2500	7729	•0080	5.0415	1.3534	1.023	245.7	
•700	15.25	5.556	3126	2766	7508	•0105	4.6659	1.369	1.022	238.6	
•800	13.60	6.349	3188	2848	7277	•0119	4.5644	1.376	1.022	231.2	
•900	12.28	7.143	3213	2858	7024	•0125	4.3169	1.379	1.022	224.1	
1.000	11.19	7.937	3217	2868	6846	•0126	4.1101	1.380	1.022	217.5	
1.200	7.749	11.902	3116	2771	6061	•0169	5.0437	1.377	1.022	192.6	
2.000	5.947	15.873	2700	2999	2220	•0087	5.0523	1.308	1.022	176.4	
3.000	4.031	23.810	2653	2209	4866	•0040	4.66610	1.339	1.023	154.8	
4.000	3.054	31.746	2347	1851	4366	•0009	4.6459	1.311	1.026	139.2	
5.000	2.458	39.683	2062	1571	3972	•0001	4.6295	1.295	1.029	127.0	
CHAMBER PRESSURE, 150 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION											
0.150	45.65	1.190	1183	639	7247	0.0000	8.9684	1.4997	1.261	244.0	
•200	38.65	1.587	1514	847	7607	•0000	6.1681	2.035	1.261	249.8	
•250	33.51	1.984	1616	1052	7814	•0000	7.5120	2.073	1.262	306.6	
•300	29.57	2.381	2092	1251	7929	•0000	6.9718	2.111	1.264	311.3	
•350	26.47	2.778	2359	1444	7988	•0000	6.5215	2.147	1.265	314.0	
•400	23.45	3.175	2553	1631	8006	•0005	6.1415	2.182	1.266	315.0	
•450	21.87	3.571	2733	1812	7986	•0016	5.8170	2.221	1.267	314.7	
•500	20.12	3.968	2881	1980	7940	•0035	5.9371	2.264	1.270	315.3	
•600	17.35	4.762	3097	2300	7782	•0068	5.0787	2.352	1.275	308.4	
•700	15.25	5.556	3291	2544	1577	•0095	4.7193	2.425	1.280	301.4	
•800	13.60	6.349	3304	2699	7393	•0113	4.64299	2.472	1.284	293.2	
•900	12.28	7.143	3356	2770	1134	•0121	4.2121	2.493	1.284	284.6	
1.000	11.19	7.937	3341	2769	6923	•0122	5.9526	2.498	1.284	276.4	
1.200	7.749	11.902	3219	2621	6120	•0103	3.3416	2.474	1.283	244.0	
2.000	5.947	15.873	3045	2382	5592	•0079	2.9807	2.427	1.280	222.4	
3.000	4.031	23.810	2695	1907	4882	•0032	2.5869	2.301	1.272	193.0	
4.000	3.054	31.746	2363	1549	4369	•0007	2.3706	2.215	1.267	172.1	
5.000	2.458	39.683	2064	1298	3972	•0000	2.2298	2.171	1.266	156.3	
CHAMBER PRESSURE, 300 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION											
0.150	45.65	1.190	1183	229	1247	0.0000	8.6565	3.020	1.379	310.6	
•200	38.65	1.587	1514	1067	7607	•0000	7.9050	3.088	1.382	265.7	
•250	33.51	1.984	1617	804	7813	•0000	7.2851	3.168	1.386	336.5	
•300	29.57	2.381	2093	1029	7929	•0000	6.7096	3.248	1.390	342.5	
•350	26.47	2.778	2344	1049	7988	•0000	6.13404	3.329	1.393	345.9	
•400	23.45	3.175	2563	1403	8006	•0005	5.9776	3.399	1.397	347.6	
•450	21.87	3.571	2702	1589	7986	•0012	5.6604	3.474	1.401	348.1	
•500	20.12	3.968	2815	1732	1956	•0025	5.3976	3.553	1.409	347.5	
•600	17.35	4.762	3125	2047	1616	•0058	4.9564	3.726	1.416	345.9	
•700	15.25	5.556	3307	2328	7625	•0087	4.6094	3.900	1.426	337.9	
•800	13.60	6.349	3393	2544	7411	•0107	4.3293	4.042	1.433	330.1	
•900	12.28	7.143	3430	2661	7193	•0117	4.0963	4.121	1.437	321.2	
1.000	11.19	7.937	3431	2667	6903	•0118	3.9046	4.140	1.438	312.0	
1.200	7.749	11.902	3247	2474	5103	•0097	3.2701	4.058	1.439	214.6	
2.000	5.947	15.873	3103	2181	5621	•0074	2.4917	3.910	1.446	249.2	
3.000	4.031	23.810	2163	1678	4892	•0021	2.45310	3.633	1.410	214.4	
4.000	3.054	31.746	2372	1245	4371	•0005	2.3183	3.474	1.400	190.2	
5.000	2.458	39.683	2064	1117	3972	•0000	2.1754	3.388	1.396	172.4	
CHAMBER PRESSURE, 600 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION											
0.150	45.65	1.190	1183	431	1247	0.0000	8.6565	4.602	1.469	330.9	
•200	38.65	1.587	1514	206	7607	•0000	7.6359	4.602	1.474	348.6	
•250	33.51	1.984	1617	731	7813	•0000	7.0041	4.949	1.481	359.6	
•300	29.57	2.381	2094	891	7929	•0000	6.5873	5.103	1.488	366.6	
•350	26.47	2.778	2347	1049	7988	•0000	6.1394	5.260	1.494	370.9	
•400	23.45	3.175	2574	1177	8006	•0004	7.0131	5.409	1.500	375.4	
•450	21.87	3.571	2713	1325	8006	•0008	7.5100	5.524	1.506	374.5	
•500	20.12	3.968	2744	1501	7908	•0019	7.2892	5.701	1.514	374.0	
•600	17.35	4.762	3208	1790	1644	•0040	4.8374	6.013	1.527	374.3	
•700	15.25	5.556	3301	2081	7607	•0077	4.5004	6.320	1.524	367.6	
•800	13.60	6.349	3401	2340	7405	•0100	4.2274	6.657	1.535	360.6	
•900	12.28	7.143	3420	2623	7230	•0111	4.0056	6.947	1.535	352.4	
1.000	11.19	7.937	3424	2712	7037	•0114	3.5173	7.322	1.565	342.0	
1.200	7.749	11.902	3374	2241	6203	•0091	3.1990	6.760	1.557	300.2	
2.000	5.947	15.873	3103	1737	5646	•0063	2.8559	6.410	1.544	271.1	
3.000	4.031	23.810	2147	1464	4702	•0023	2.4472	5.862	1.520	214.4	
4.000	3.054	31.746	2301	1197	4312	•0004	2.2202	5.572	1.509	204.7	
5.000	2.458	39.683	2070	773	3972	•0000	2.0202	5.405	1.498	160.1	

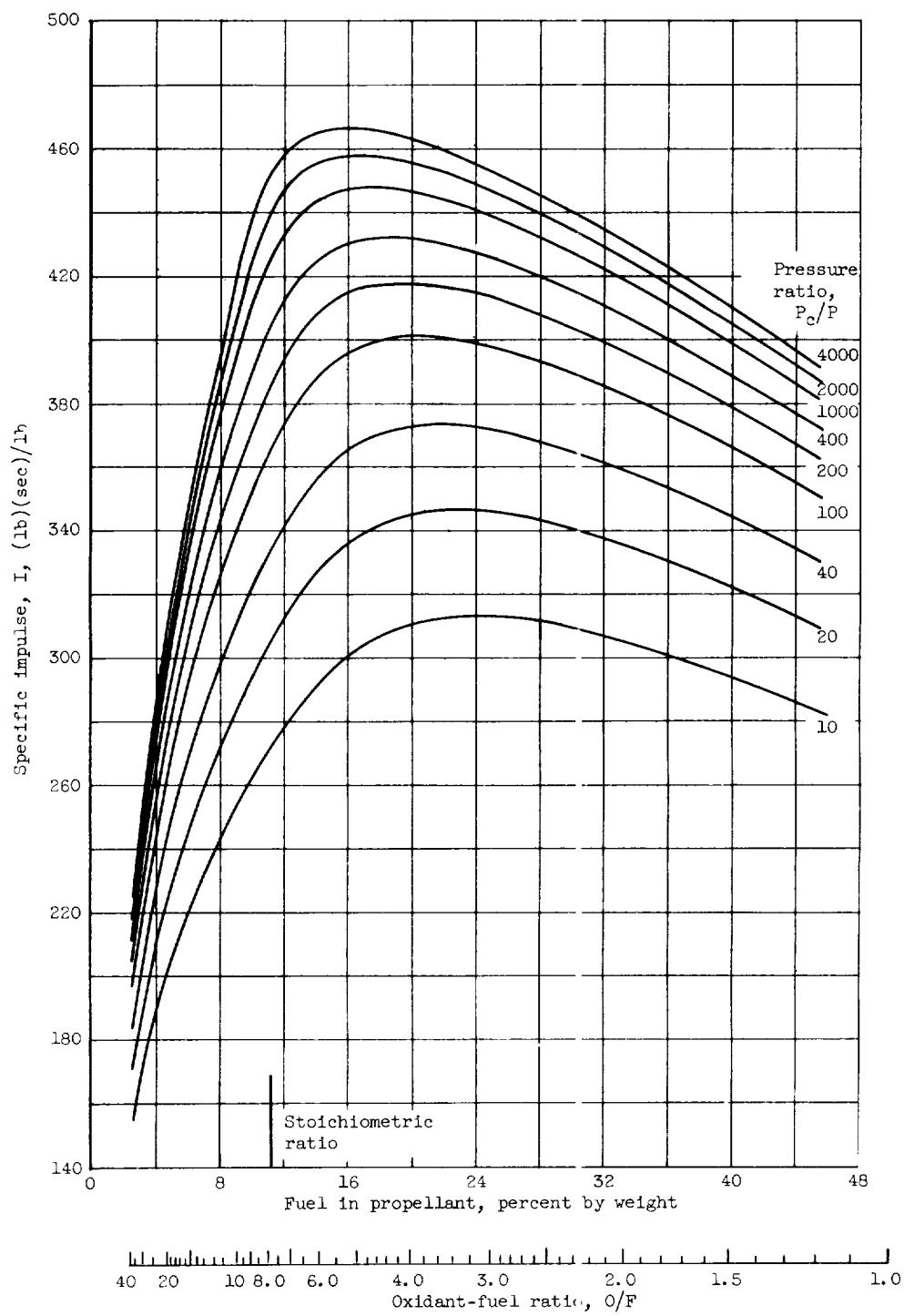
TABLE V. - Concluded. SUMMARY OF COMBUSTION PARAMETERS, CHARACTERISTIC VELOCITY, AND PERFORMANCE FOR EXPANSION TO SEA LEVEL FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

Equiv-alence ratio, R _{2(0)/H}	Fuel, percent by weight	Oxidant-weight ratio, O/F	Com-bus-tion tem-pera-ture, T _c , °K	Exit tem-perature, T _e , °K	Charac-teristic veloci-ty, c, ft/sec	En-trap-ty, s, cal/(g)(°K)	Area ratio, ε	Coeffi-cient of thrust, C _F	Specific impulse, I, (lb){sec}
CHAMBER PRESSURE, 60 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	819	7247	9.3807	1.244	1.038	233.7
*200	38.65	1.587	1514	1075	7607	8.5172	1.256	1.035	244.7
*250	33.21	1.984	1816	1315	7611	7.8147	1.267	1.033	250.8
*300	29.57	2.381	2089	1540	7916	7.2340	1.278	1.032	253.8
*350	26.47	2.778	2329	1741	7948	6.6711	1.286	1.030	254.6
*400	23.95	3.175	2531	1912	7922	6.3190	1.292	1.030	253.5
*450	21.87	3.571	2696	2053	7856	6.067	1.297	1.029	251.3
*500	20.12	3.968	2826	2166	7763	5.722	1.301	1.029	248.2
*600	17.35	4.762	3015	2330	7542	5.2413	1.307	1.028	241.0
*700	15.25	5.556	3128	2429	7304	4.8859	1.310	1.028	233.3
*800	13.60	6.349	3188	2684	7070	4.6544	1.312	1.028	225.8
*900	12.28	7.143	3213	2700	6850	4.4559	1.313	1.028	218.8
1,000	11.19	7.937	3217	2714	6648	4.1101	1.313	1.027	212.3
1,100	7.749	11.903	3116	2433	5891	3.4711	1.313	1.026	168.1
2,000	5.927	15.075	2966	2304	4601	3.0753	1.311	1.028	172.5
3,000	4.031	23.810	2692	2040	4766	2.6610	1.305	1.028	152.3
4,000	3.054	31.746	2597	1789	4316	2.4399	1.298	1.029	138.1
5,000	2.655	39.683	2602	1554	3954	2.0462	1.292	1.030	126.6
CHAMBER PRESSURE, 150 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	639	7247	8.9784	1.2997	1.261	284.0
*200	38.65	1.587	1514	847	7607	8.1681	1.3033	1.261	298.2
*250	33.21	1.984	1816	1052	7812	7.5120	1.3072	1.263	306.5
*300	29.57	2.381	2089	1240	7921	6.9718	1.3110	1.264	311.2
*350	26.47	2.778	2329	1430	7961	6.5115	1.3142	1.265	319.1
*400	23.95	3.175	2531	1792	7500	6.1615	1.3168	1.267	313.0
*450	21.87	3.571	2753	1730	7699	5.8170	1.3189	1.268	311.2
*500	20.12	3.968	2881	1846	7641	5.5211	1.3202	1.268	308.3
*600	17.35	4.762	3097	2019	7621	5.0537	1.3228	1.269	300.7
*700	15.25	5.556	3231	2126	7395	4.7193	1.3242	1.270	291.9
*800	13.60	6.349	3304	2190	7166	4.4499	1.3251	1.271	283.0
*900	12.28	7.143	3336	2219	6947	4.1519	1.3260	1.271	274.4
1,000	11.19	7.937	3341	2226	6743	3.9526	1.3258	1.271	266.3
1,500	7.749	11.903	3249	2140	5965	3.3416	1.3255	1.271	235.6
2,000	5.927	15.075	3045	2009	5458	2.9637	1.3244	1.270	215.5
3,000	4.031	23.810	2695	1745	4796	2.5659	1.3219	1.269	189.2
4,000	3.054	31.746	2593	1498	4292	2.3705	1.3192	1.268	170.6
5,000	2.655	39.683	2606	1284	3958	2.0229	1.3166	1.267	155.8
CHAMBER PRESSURE, 300 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	529	7247	8.6522	1.3020	1.379	310.6
*200	38.65	1.587	1514	702	7607	7.9040	1.3088	1.386	326.7
*250	33.21	1.984	1817	884	7812	7.4531	1.3167	1.386	336.5
*300	29.57	2.381	2093	1057	7923	6.7676	1.3247	1.390	342.2
*350	26.47	2.778	2344	1223	7969	6.3474	1.3319	1.394	345.1
*400	23.95	3.175	2565	1376	7966	5.9772	1.3380	1.397	345.8
*450	21.87	3.571	2755	1511	7926	5.6634	1.3451	1.399	344.7
*500	20.12	3.968	2813	1627	8050	5.3576	1.3571	1.401	342.3
*600	17.35	4.762	3122	1803	7675	4.9534	1.3550	1.404	335.0
*700	15.25	5.556	3307	1922	7401	4.6074	1.3567	1.406	326.1
*800	13.60	6.349	3393	1990	7257	4.3213	1.3590	1.408	316.6
*900	12.28	7.143	3420	2022	7019	4.0513	1.3602	1.408	307.2
1,000	11.19	7.937	3437	2051	6813	3.8016	1.3607	1.407	298.3
1,500	7.749	11.903	3249	1940	6017	3.2711	1.3597	1.408	263.4
2,000	5.927	15.075	3103	1804	5496	2.9171	1.3569	1.406	240.4
3,000	4.031	23.810	2723	1540	4816	2.5310	1.3503	1.403	210.0
4,000	3.054	31.746	2574	1304	4331	2.3113	1.3439	1.400	168.7
5,000	2.655	39.683	2604	1107	3760	2.0174	1.3380	1.397	171.9
CHAMBER PRESSURE, 600 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	431	7247	8.3446	1.3020	1.469	330.9
*200	38.65	1.587	1514	585	7607	7.6519	1.3082	1.474	348.6
*250	33.21	1.984	1817	617	7813	7.0511	1.3169	1.481	359.6
*300	29.57	2.381	2074	689	7924	6.5515	1.3204	1.488	366.4
*350	26.47	2.778	2347	1037	7974	6.1514	1.3252	1.494	370.3
*400	23.95	3.175	2514	1101	7705	5.8111	1.3284	1.499	371.8
*450	21.87	3.571	2713	1310	7947	5.5110	1.3367	1.504	371.5
*500	20.12	3.968	2794	1424	7890	5.2212	1.3391	1.508	369.7
*600	17.35	4.762	3003	1601	7722	4.8317	1.3370	1.513	353.3
*700	15.25	5.556	3281	1724	7522	4.5012	1.3521	1.517	354.6
*800	13.60	6.349	3465	1801	7300	4.2214	1.3576	1.519	344.9
*900	12.28	7.143	3510	1844	7089	4.0016	1.3606	1.520	335.0
1,000	11.19	7.937	3524	1851	6882	3.8119	1.3619	1.521	325.3
1,500	7.749	11.903	3514	1750	6071	3.41910	1.3887	1.519	285.7
2,000	5.927	15.075	3123	1610	5550	2.8519	1.3810	1.517	264.0
3,000	4.031	23.810	2747	1302	4835	2.4414	1.3867	1.510	226.9
4,000	3.054	31.746	2551	1122	4343	2.2512	1.3921	1.505	205.1
5,000	2.655	39.683	2603	945	3760	2.0120	1.3953	1.499	184.6



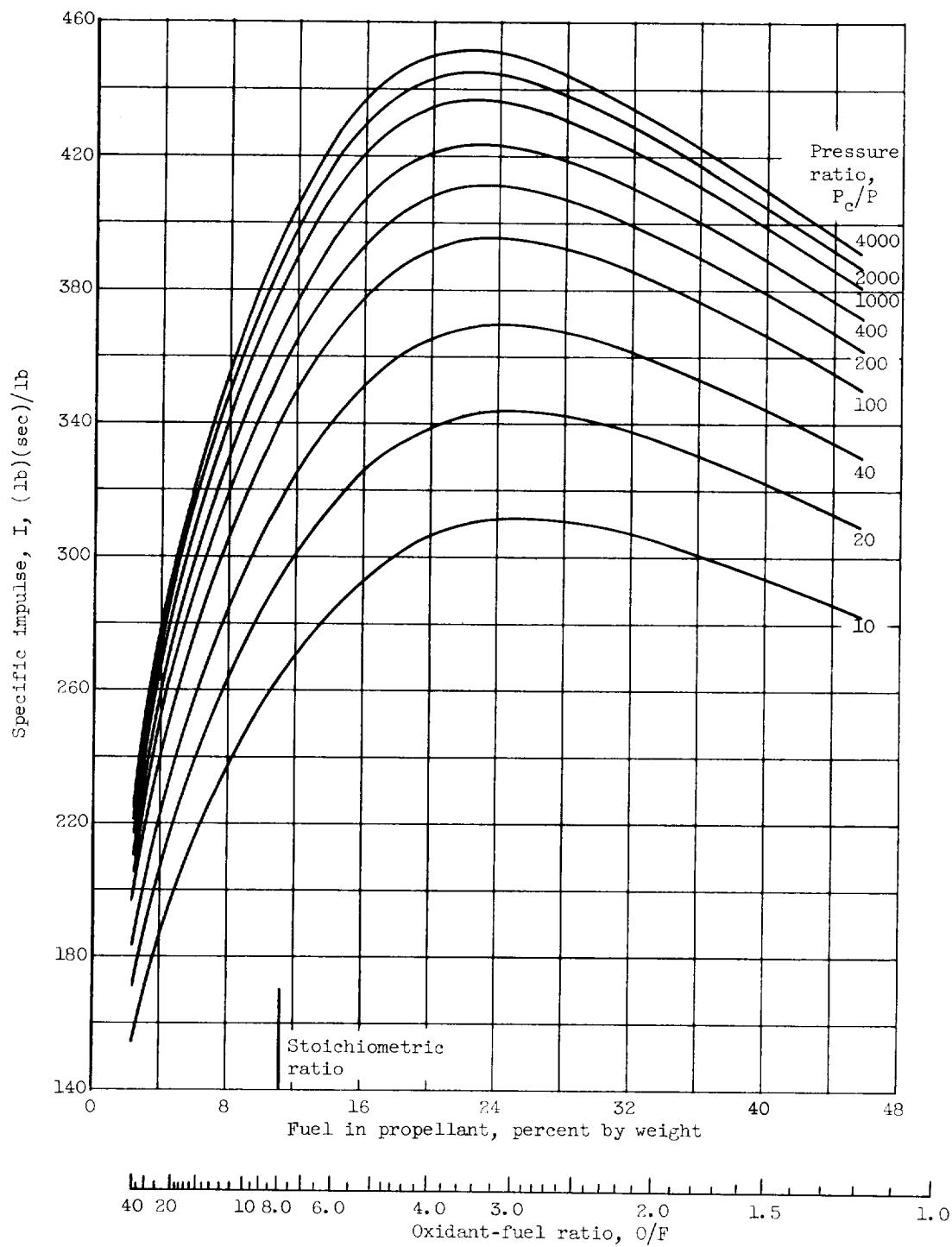
(a) Chamber pressure, 60 pounds per square inch absolute; frozen composition during expansion.

Figure 1. - Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



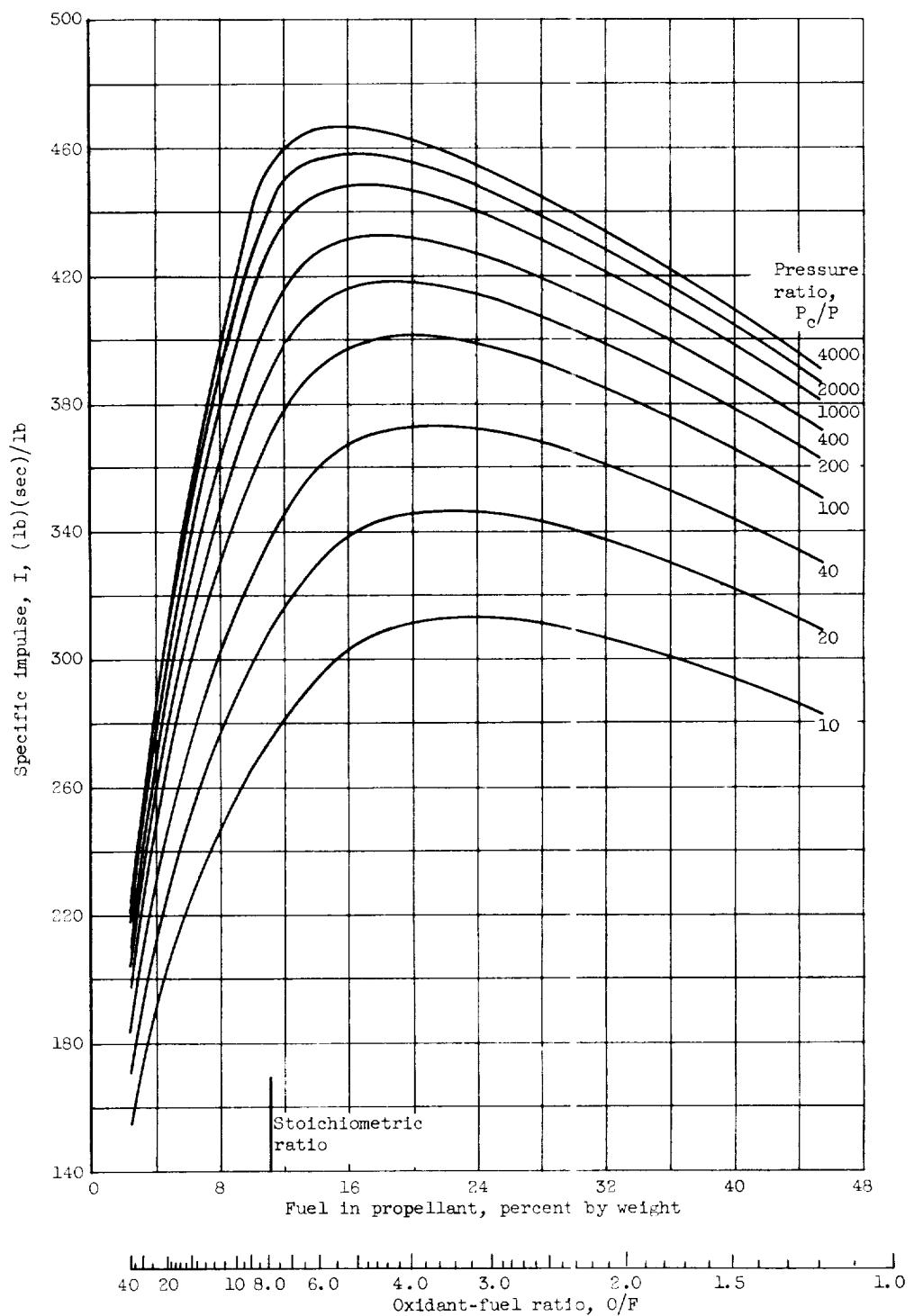
(b) Chamber pressure, 60 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



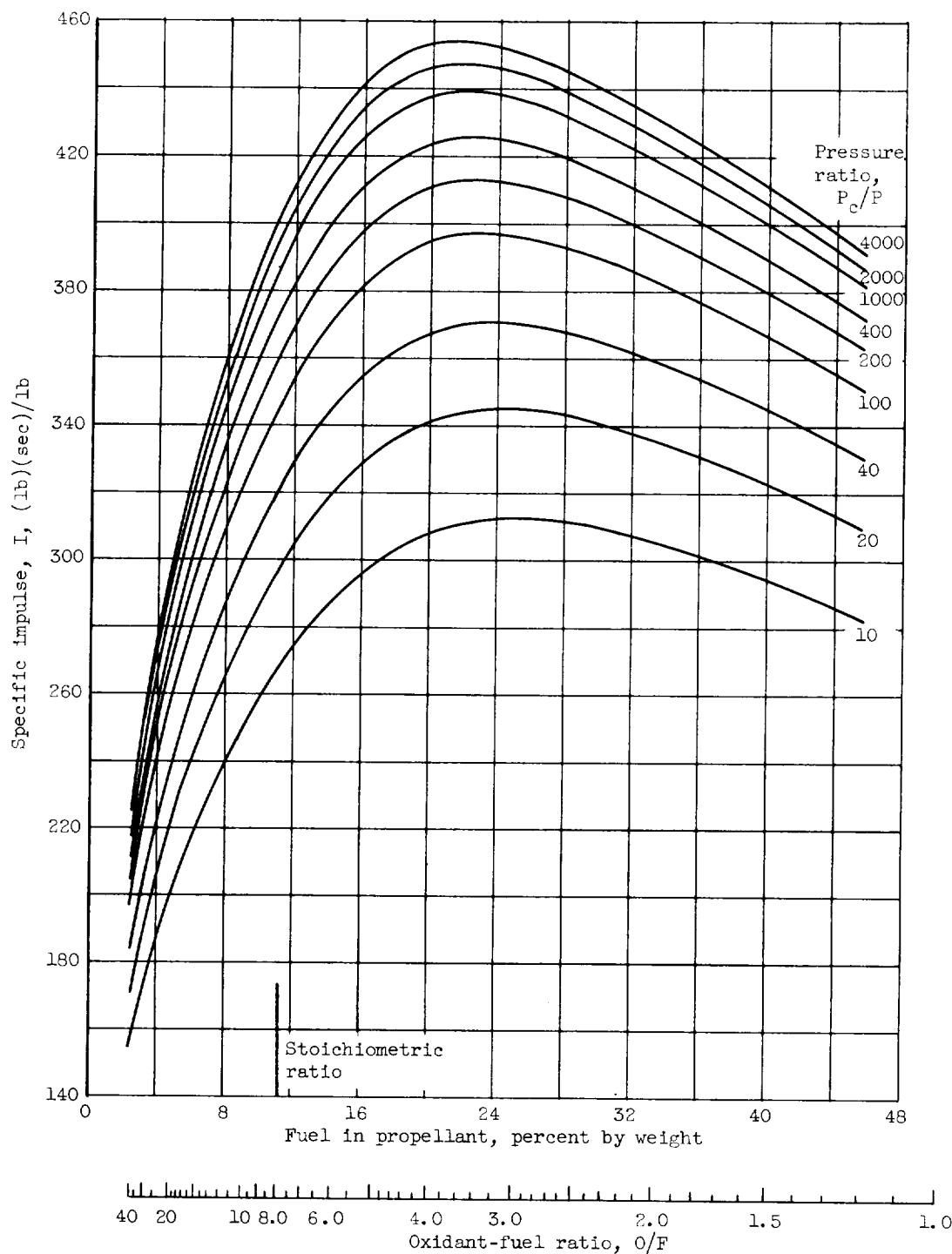
(c) Chamber pressure, 150 pounds per square inch absolute; frozen composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



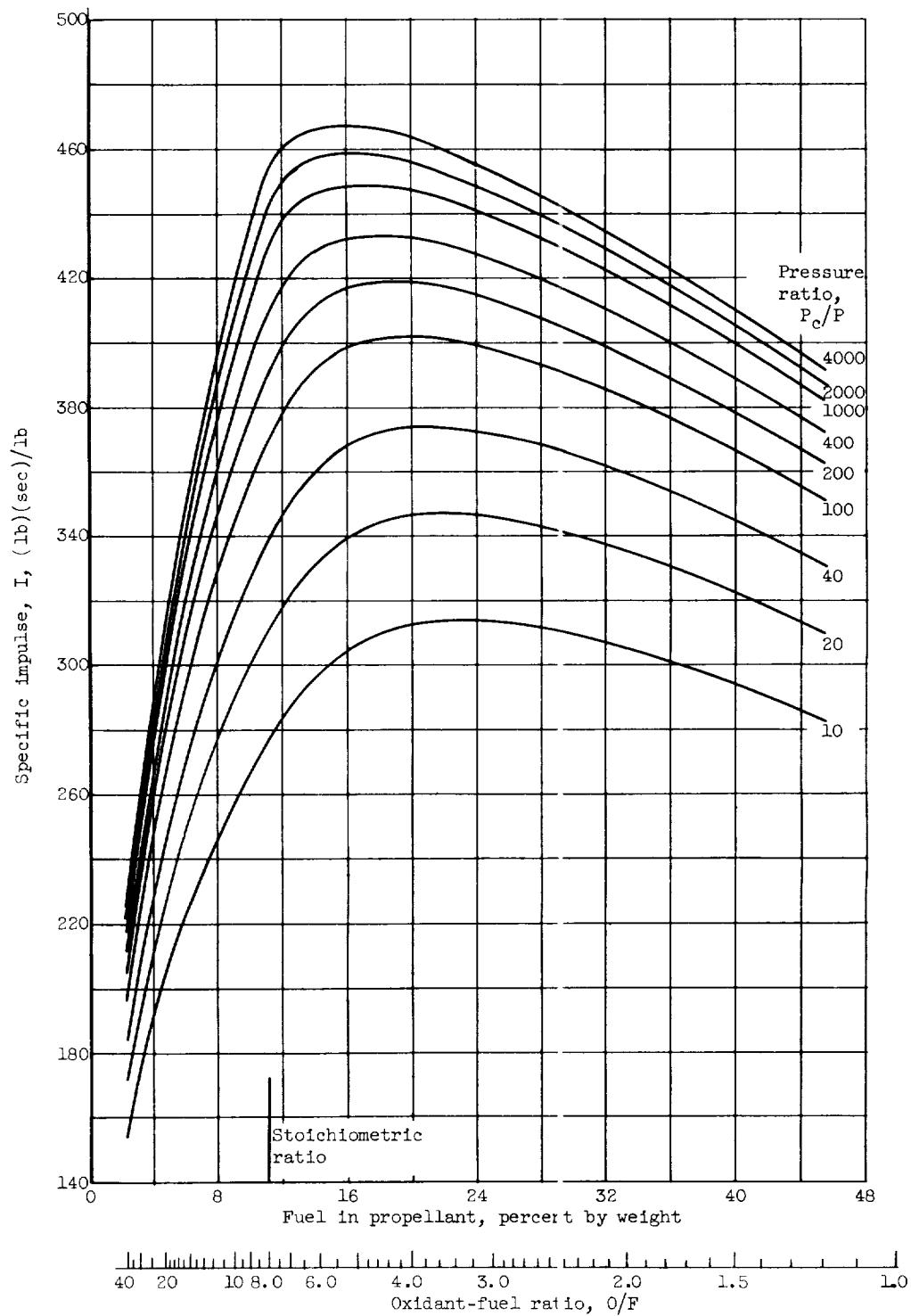
(d) Chamber pressure, 150 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



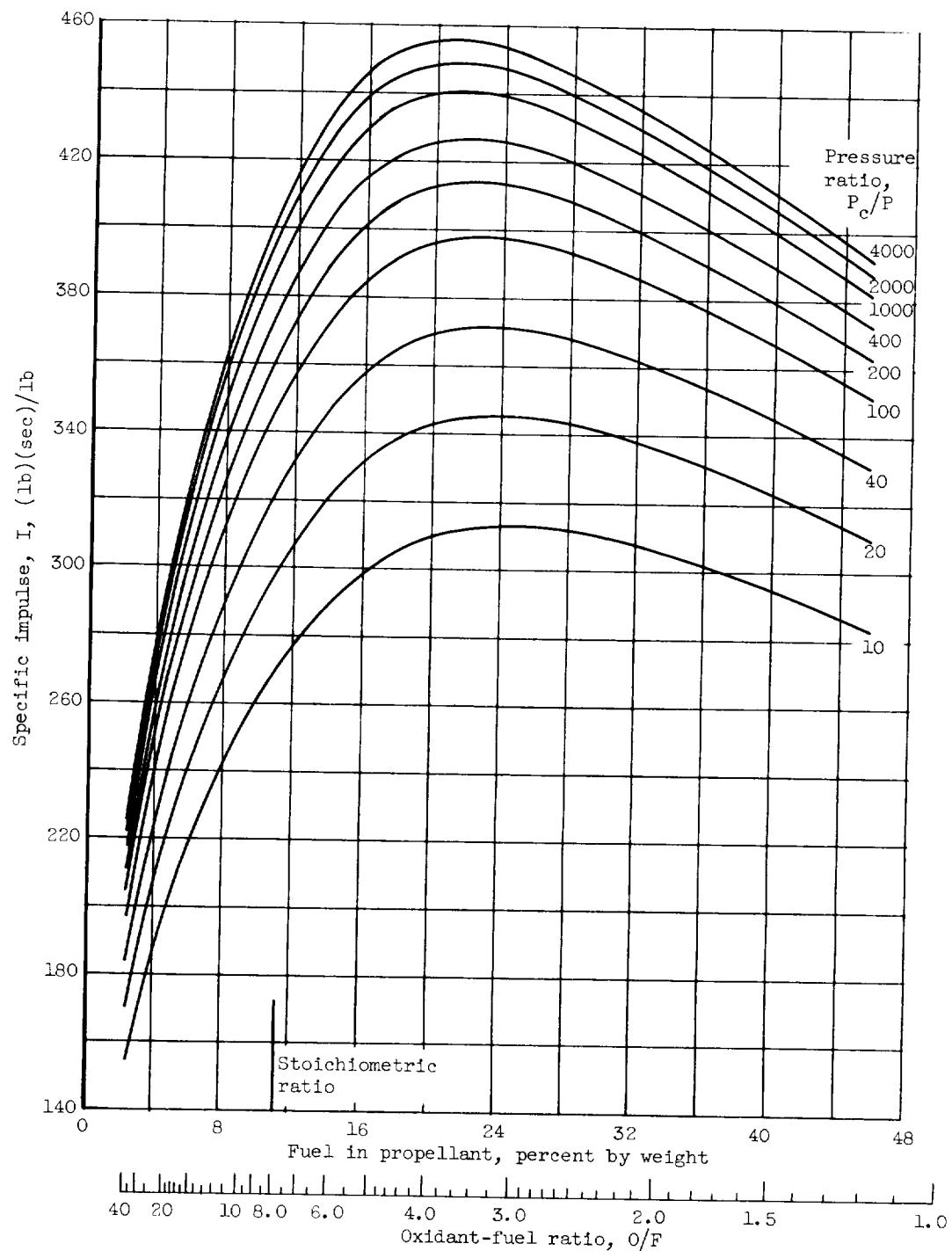
(e) Chamber pressure, 300 pounds per square inch absolute; frozen composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



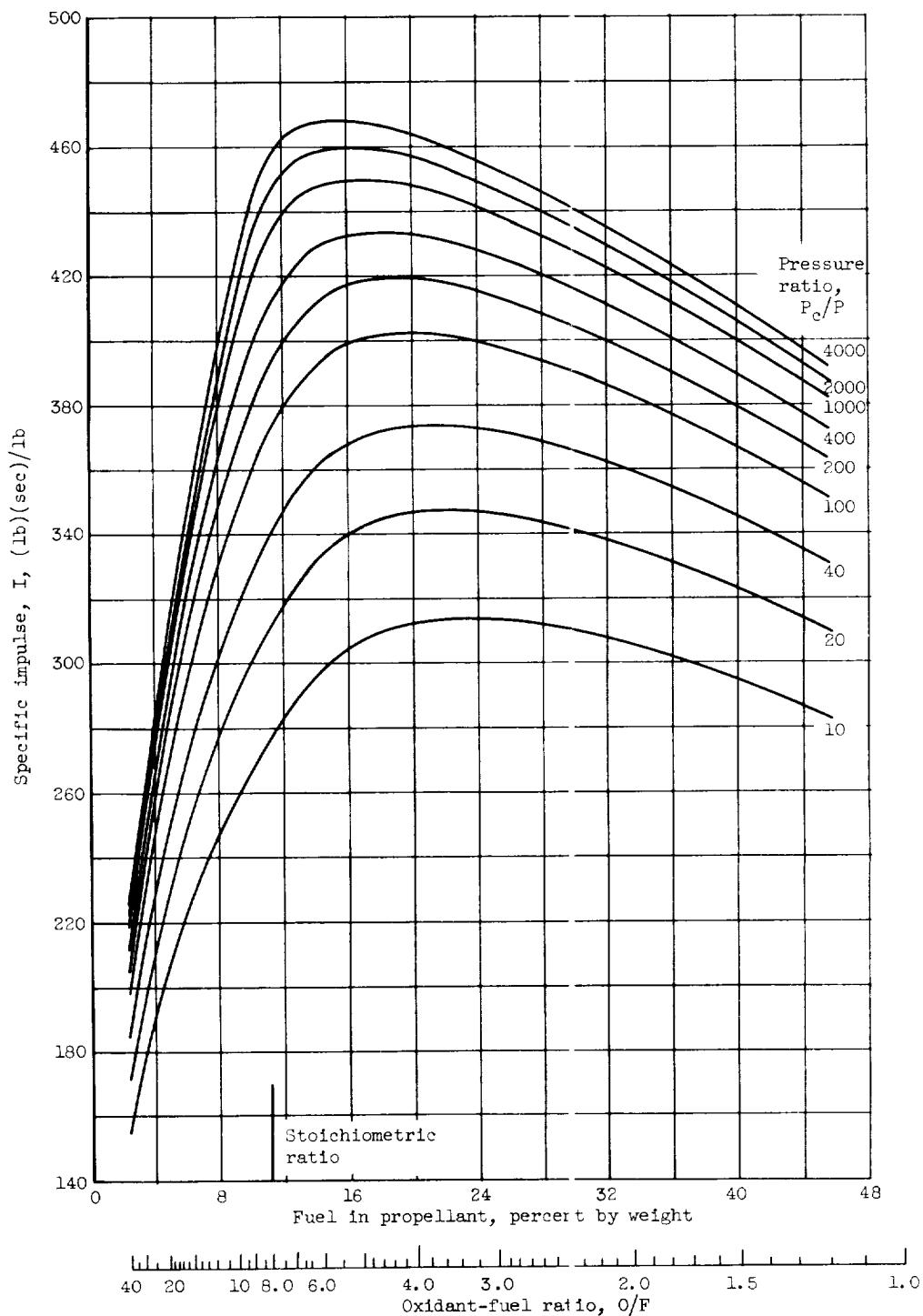
(f) Chamber pressure, 300 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



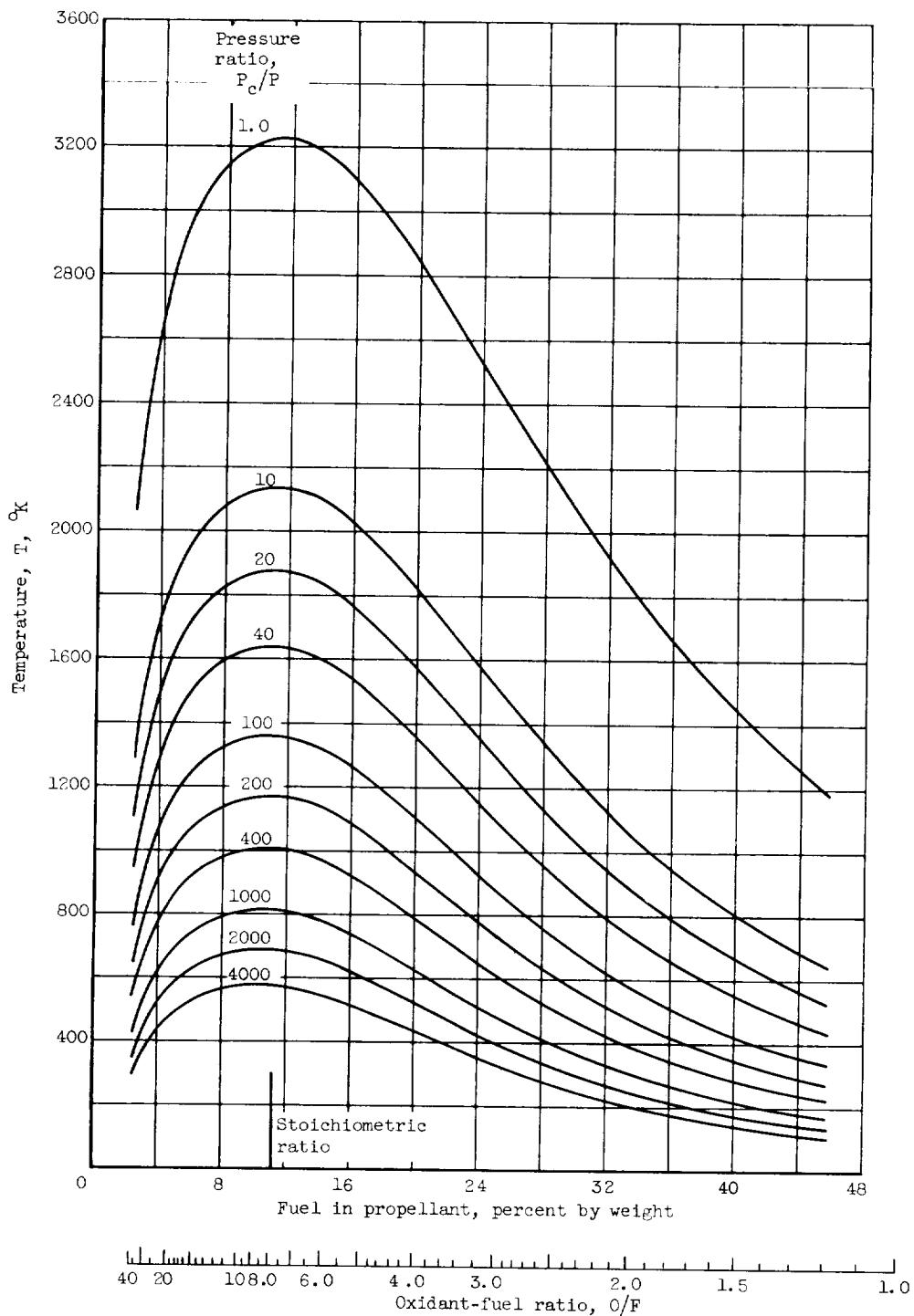
(g) Chamber pressure, 600 pounds per square inch absolute; frozen composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



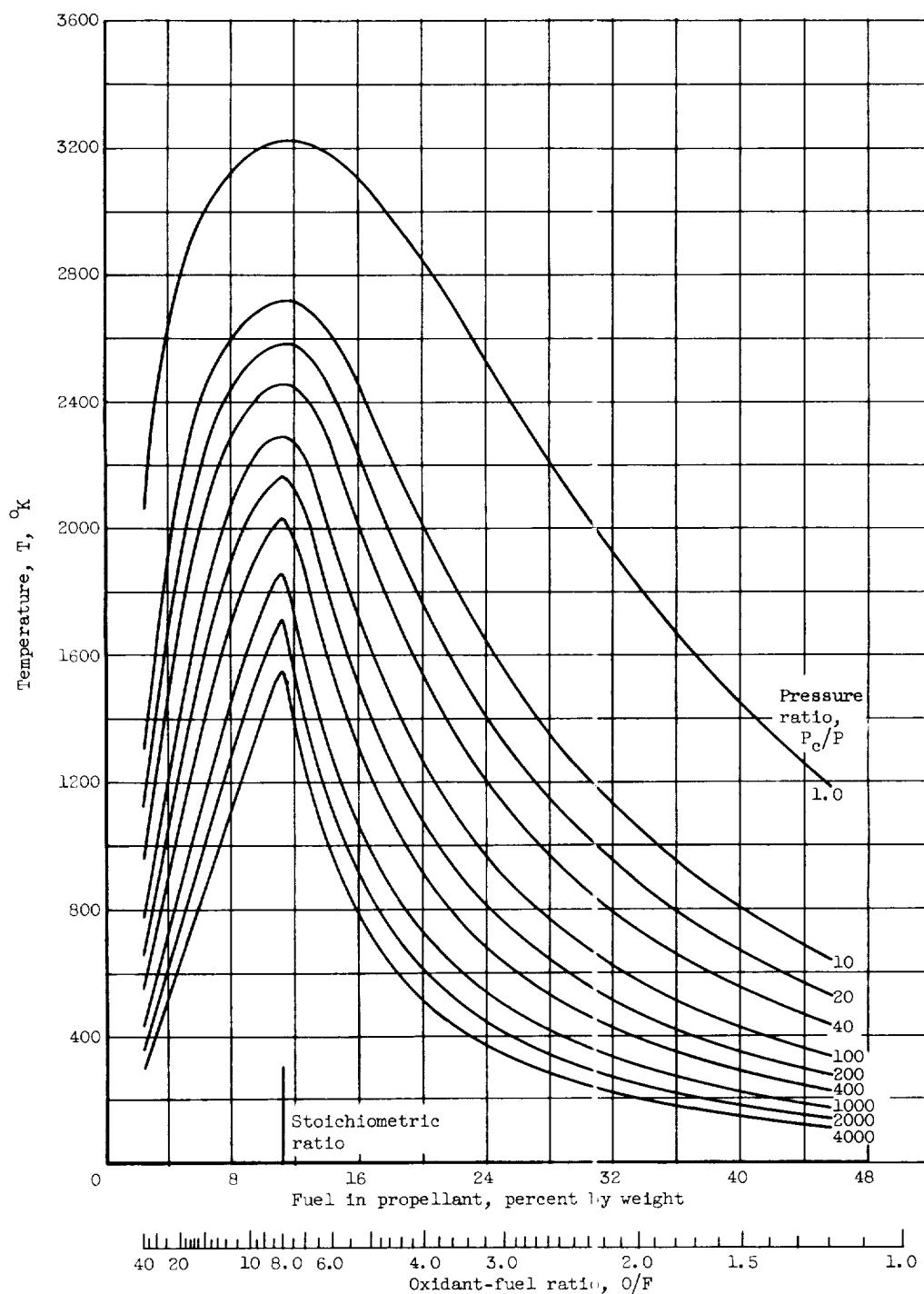
(h) Chamber pressure, 600 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 1. - Concluded. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



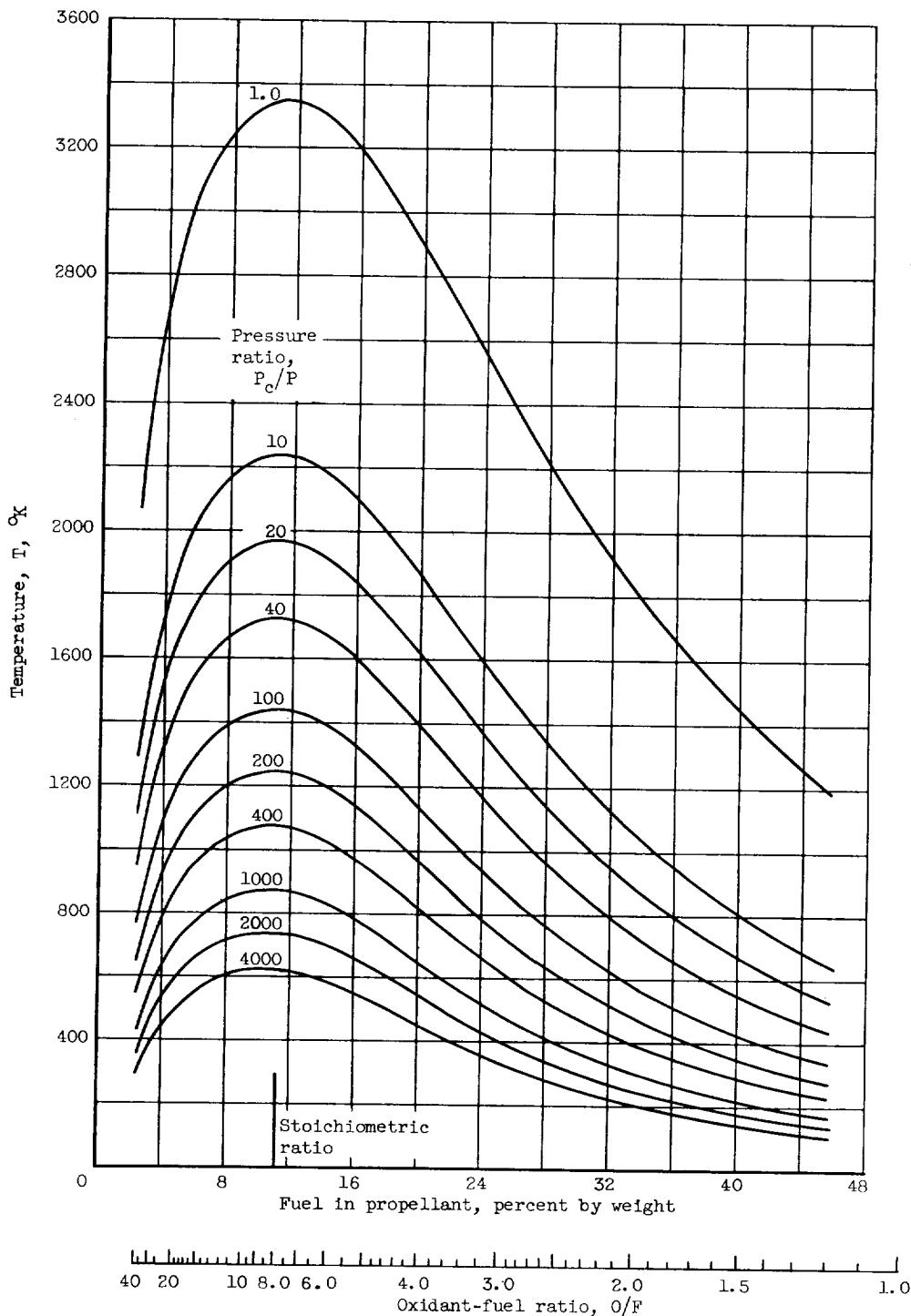
(a) Chamber pressure, 60 pounds per square inch absolute; frozen composition during expansion.

Figure 2. - Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



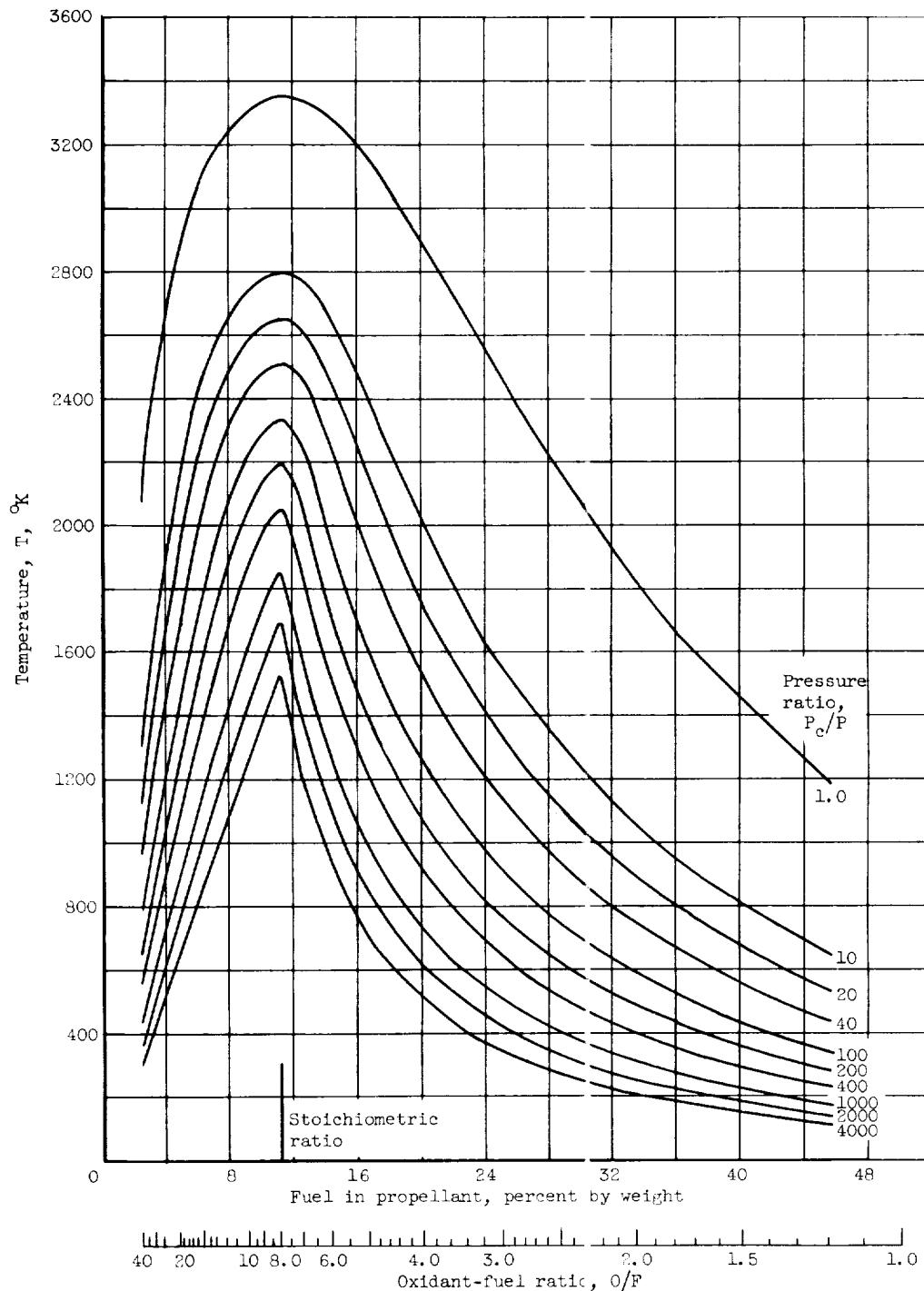
(b) Chamber pressure, 60 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



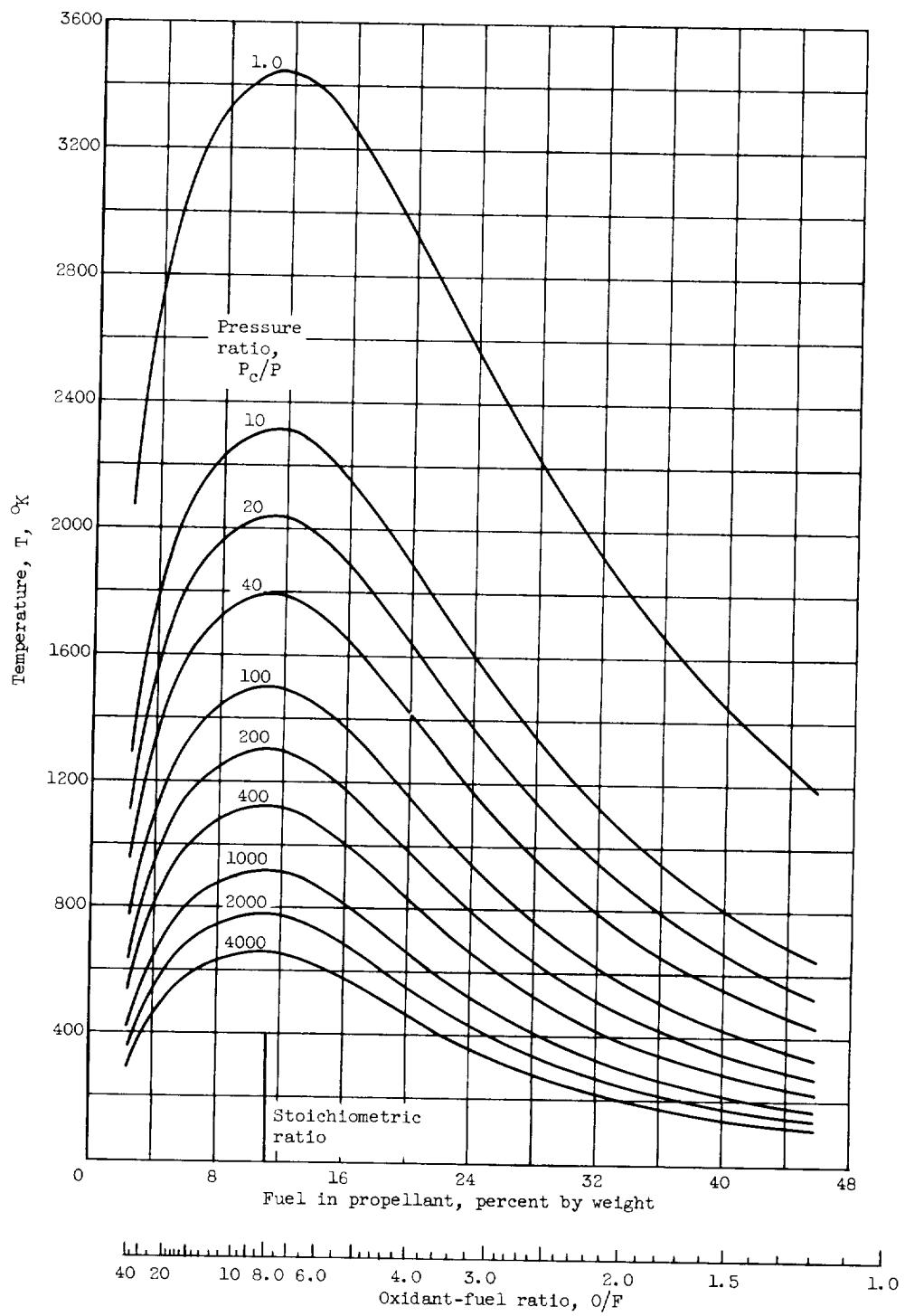
(c) Chamber pressure, 150 pounds per square inch absolute; frozen composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



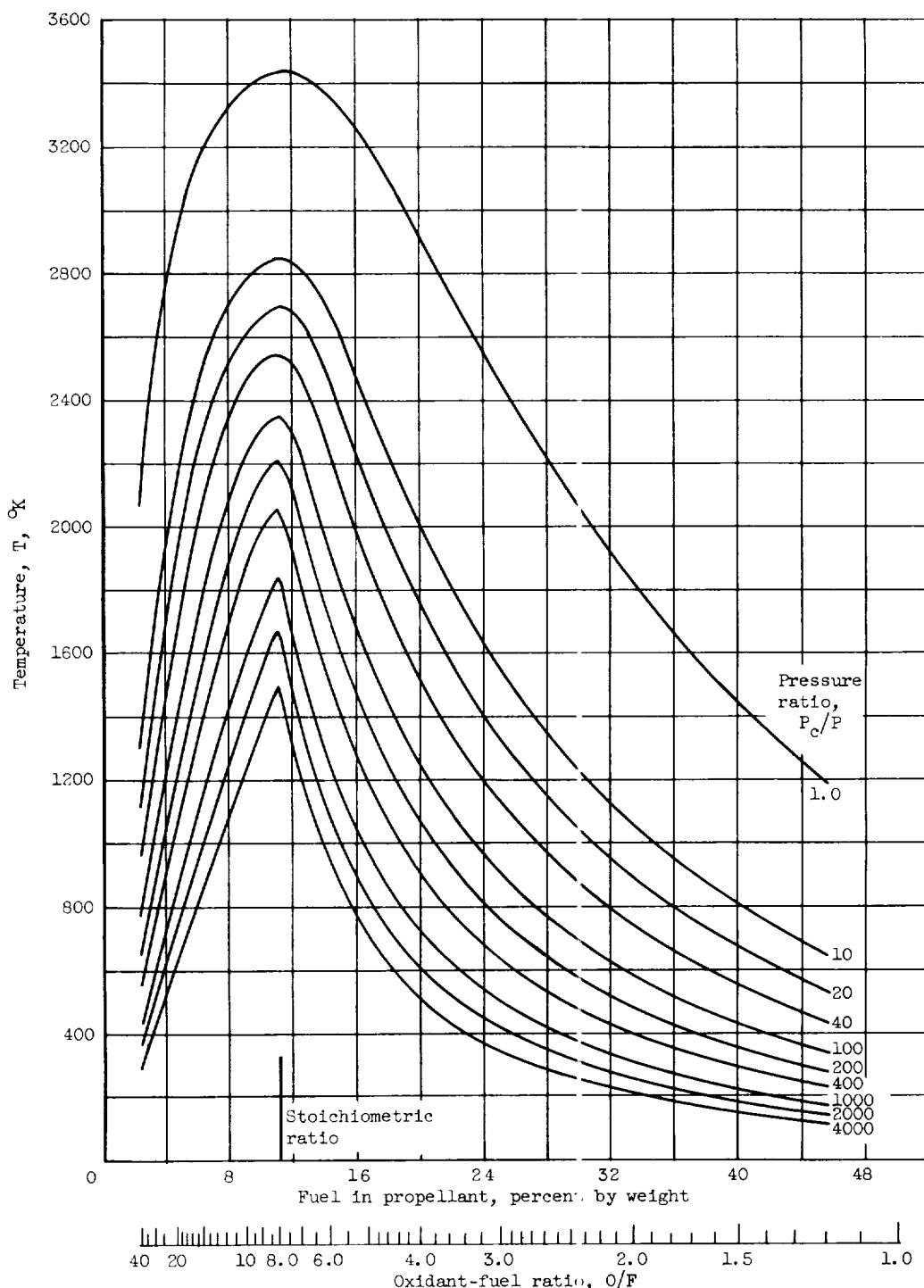
(d) Chamber pressure, 150 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



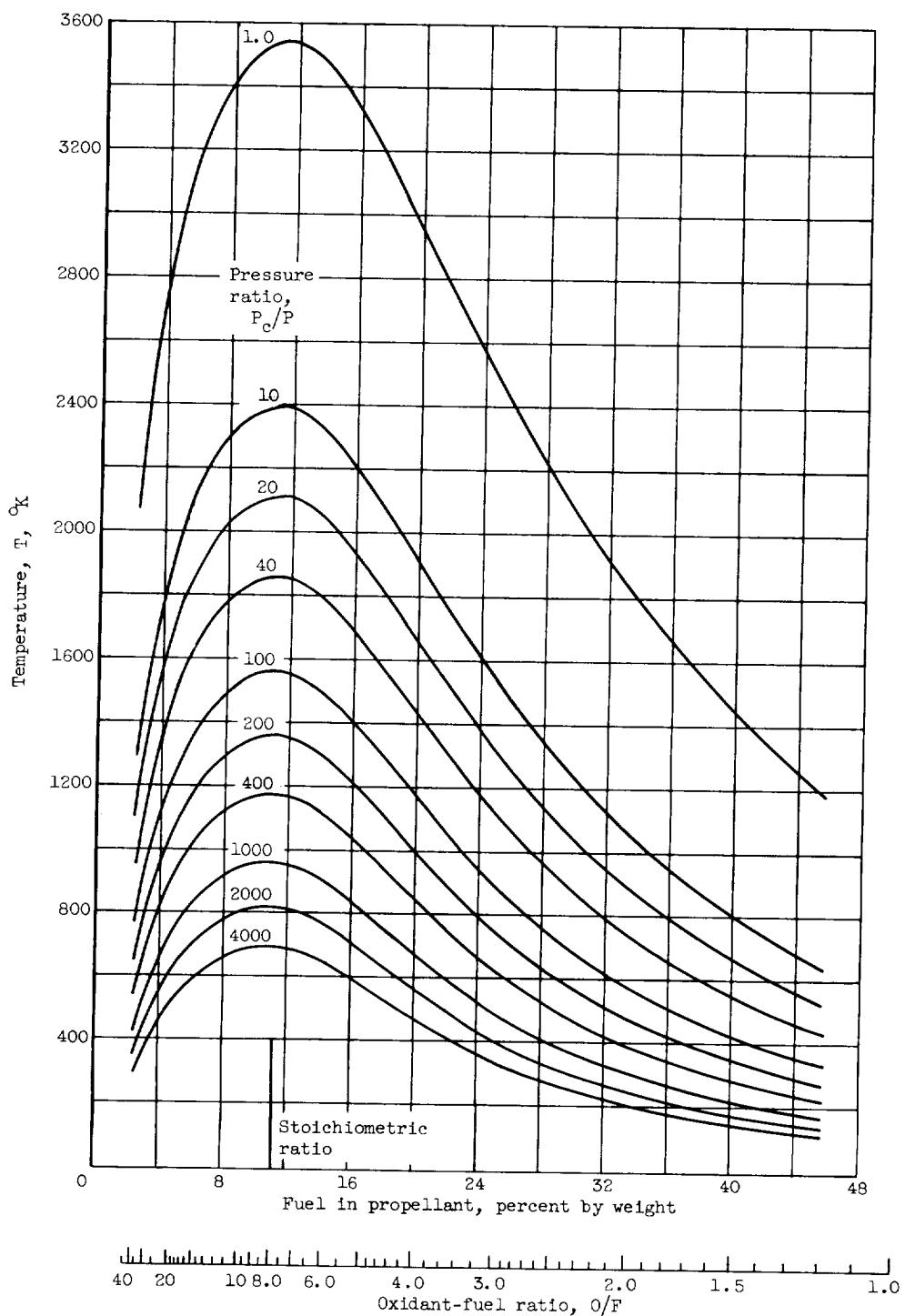
(e) Chamber pressure, 300 pounds per square inch absolute; frozen composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



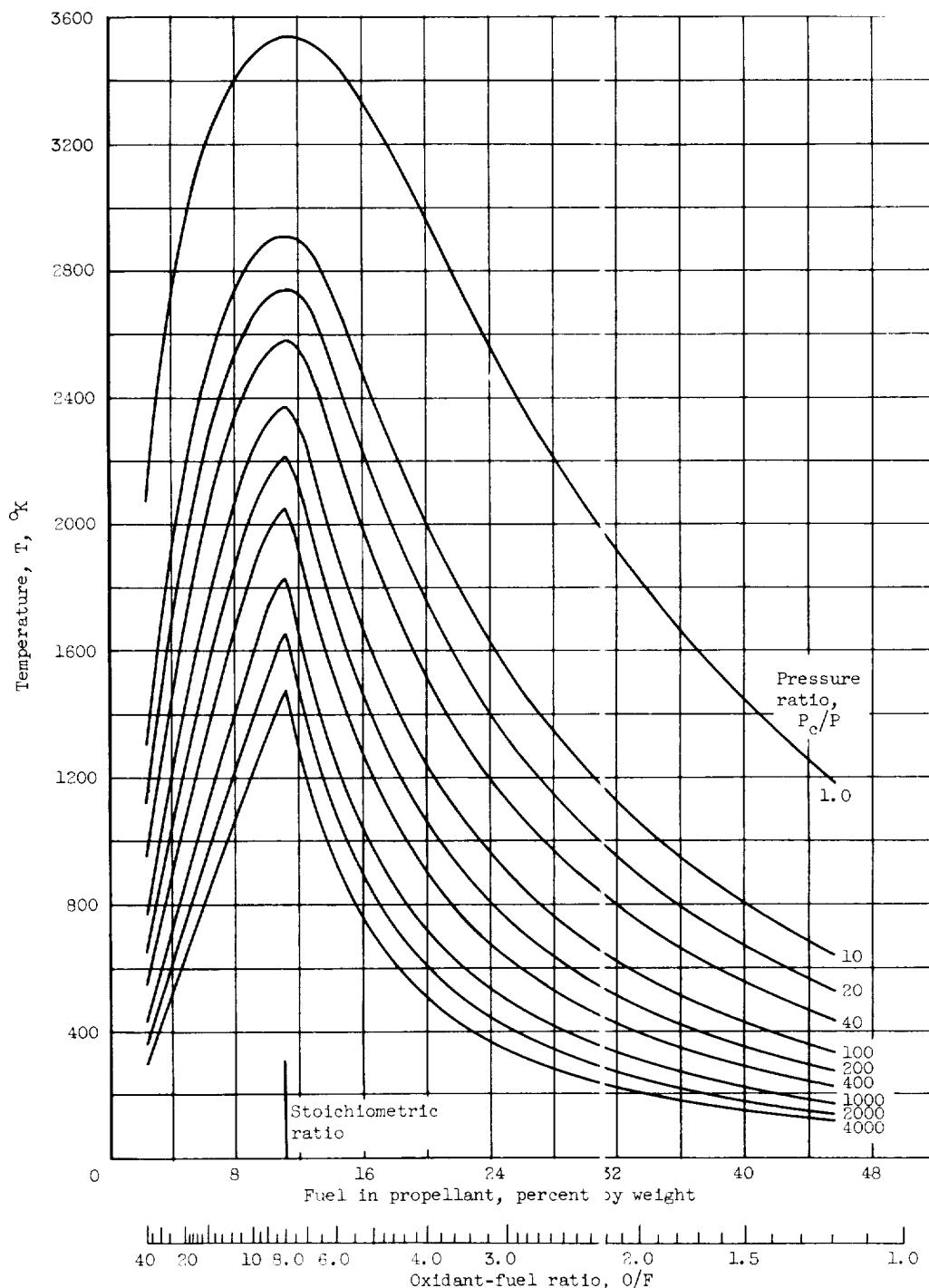
(f) Chamber pressure, 300 pounds per square inch absolute; equilibrium composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



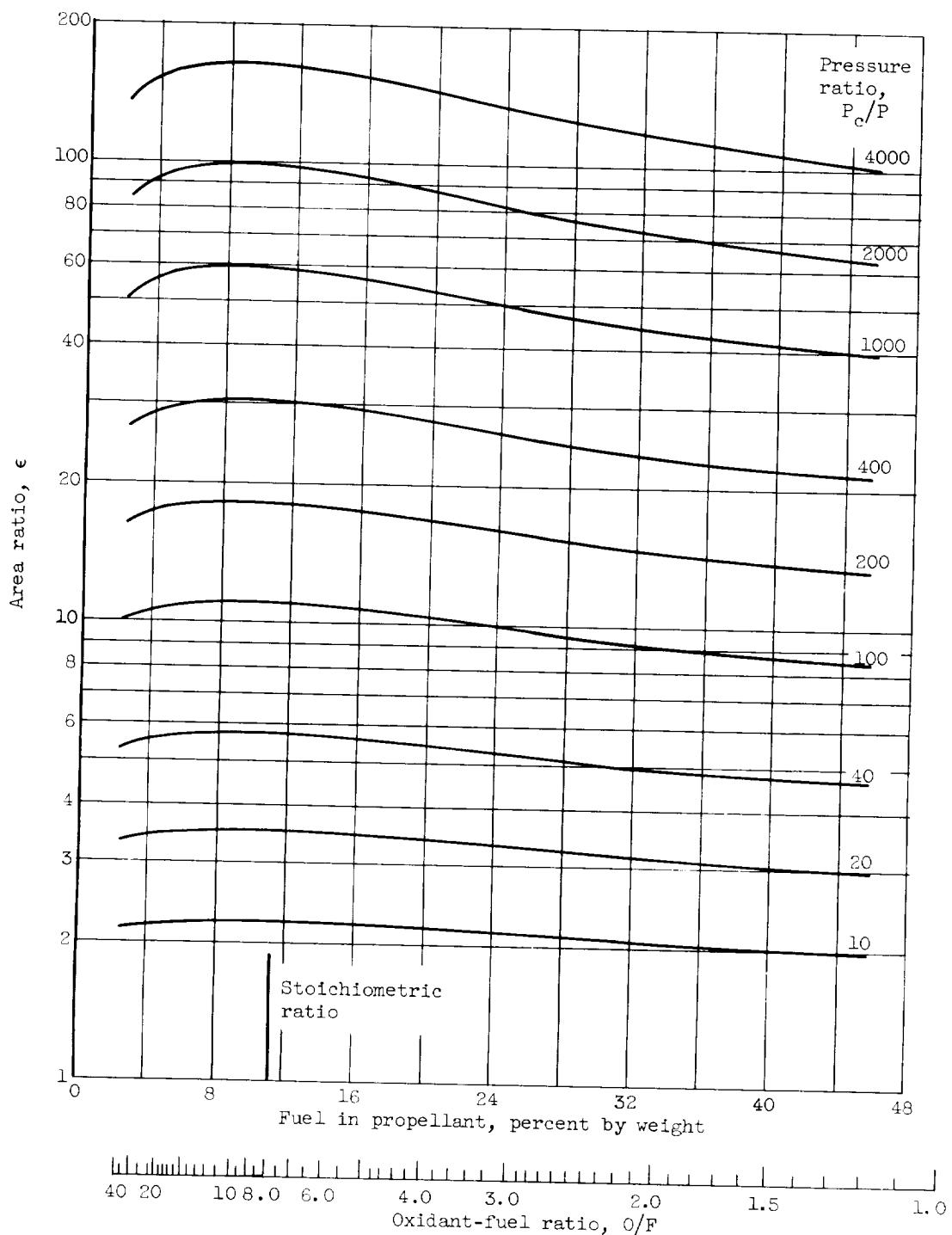
(g) Chamber pressure, 600 pounds per square inch absolute;
frozen composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



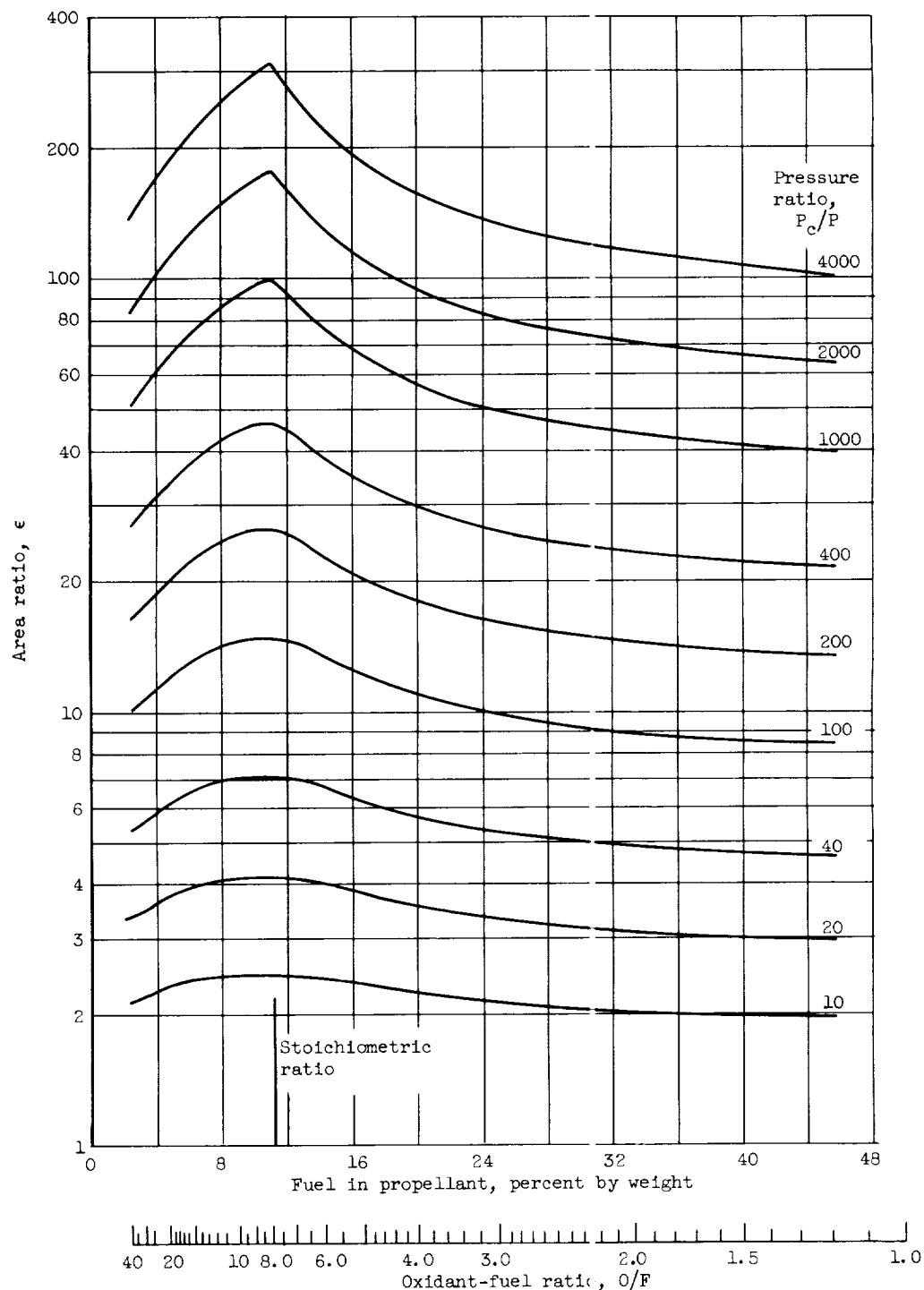
(n) Chamber pressure, 600 pounds per square inch absolute; equilibrium composition during expansion.

Figure 2. - Concluded. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



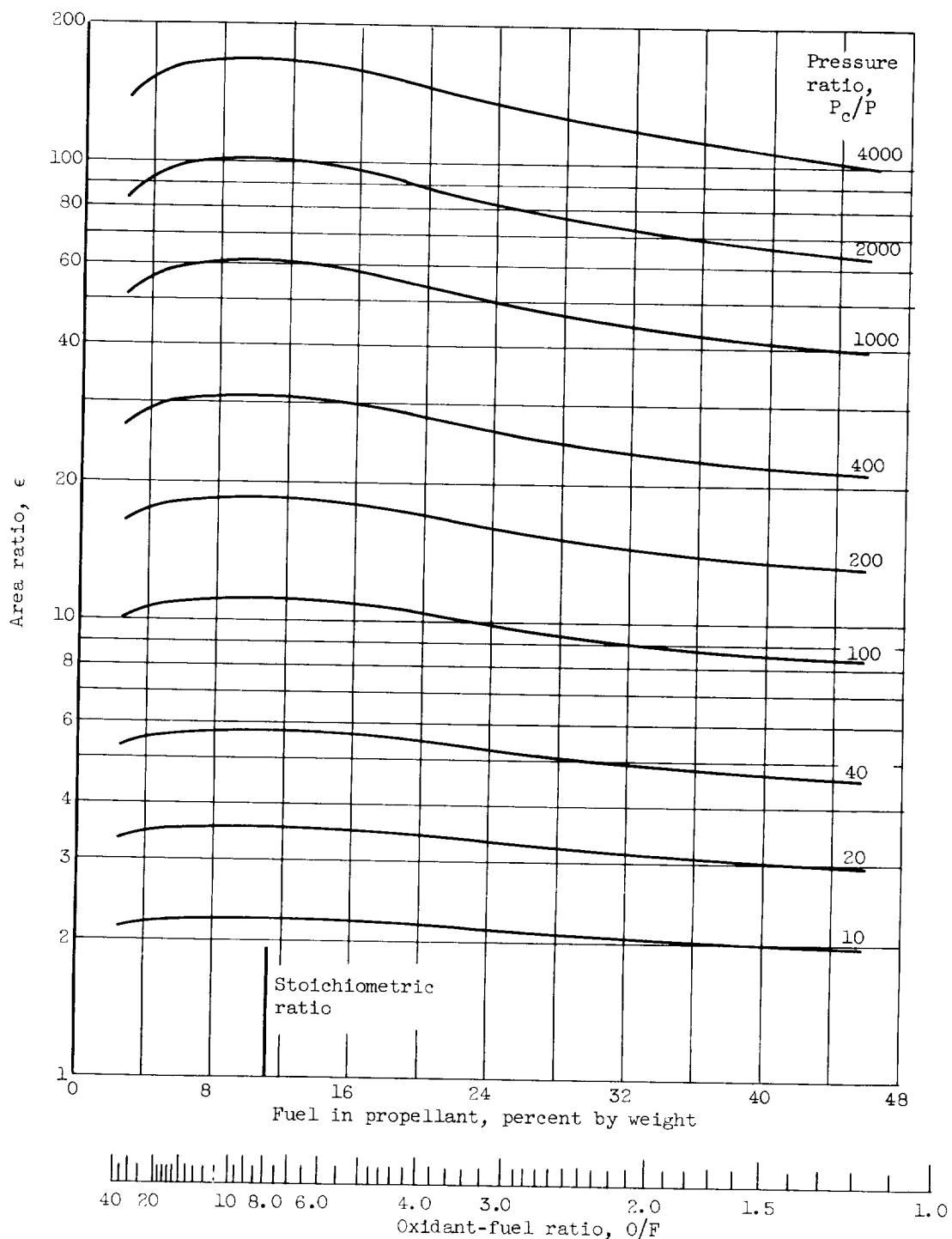
(a) Chamber pressure, 60 pounds per square inch absolute;
frozen composition during expansion.

Figure 3. - Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



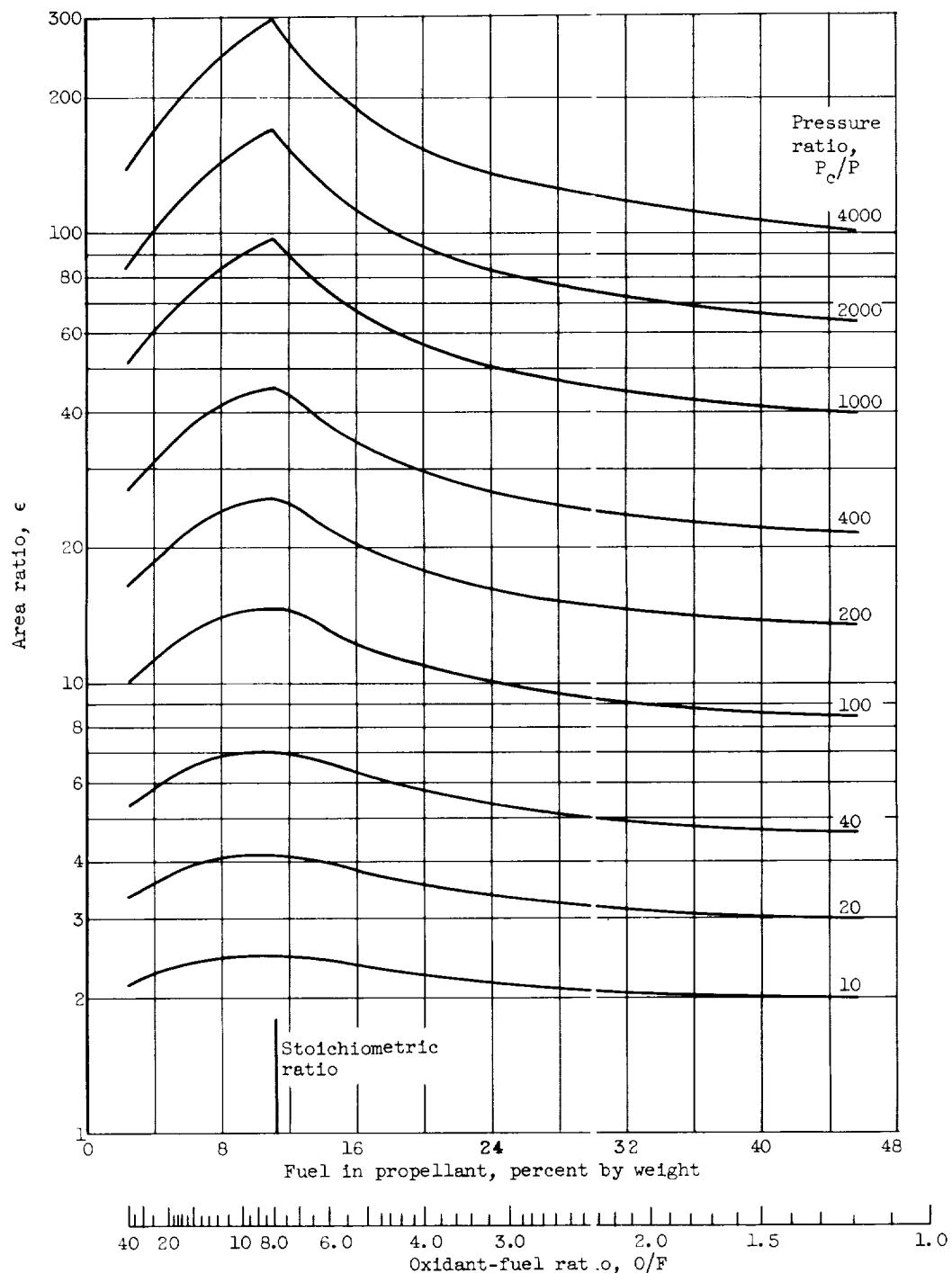
(b) Chamber pressure, 60 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



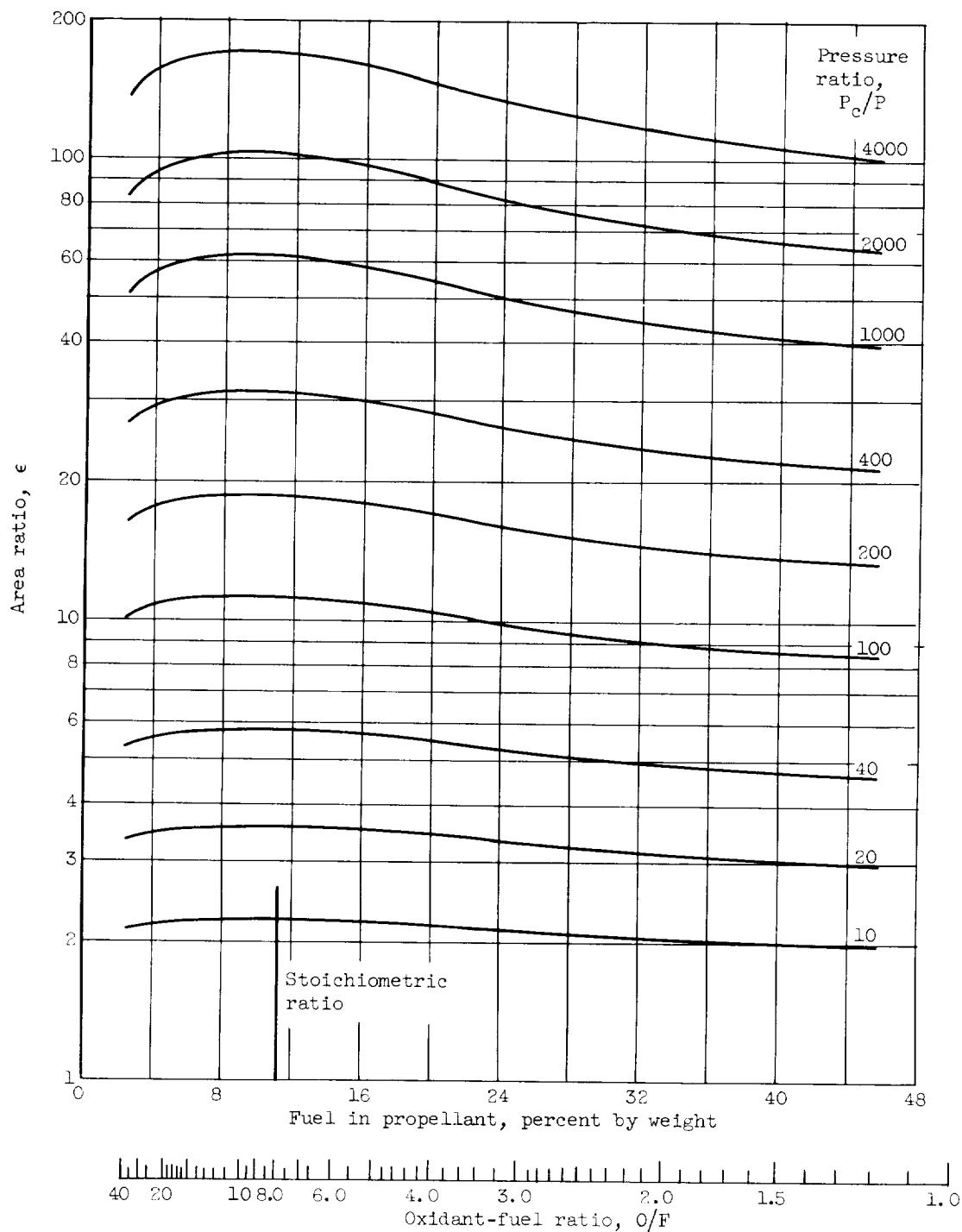
(c) Chamber pressure, 150 pounds per square inch absolute; frozen composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



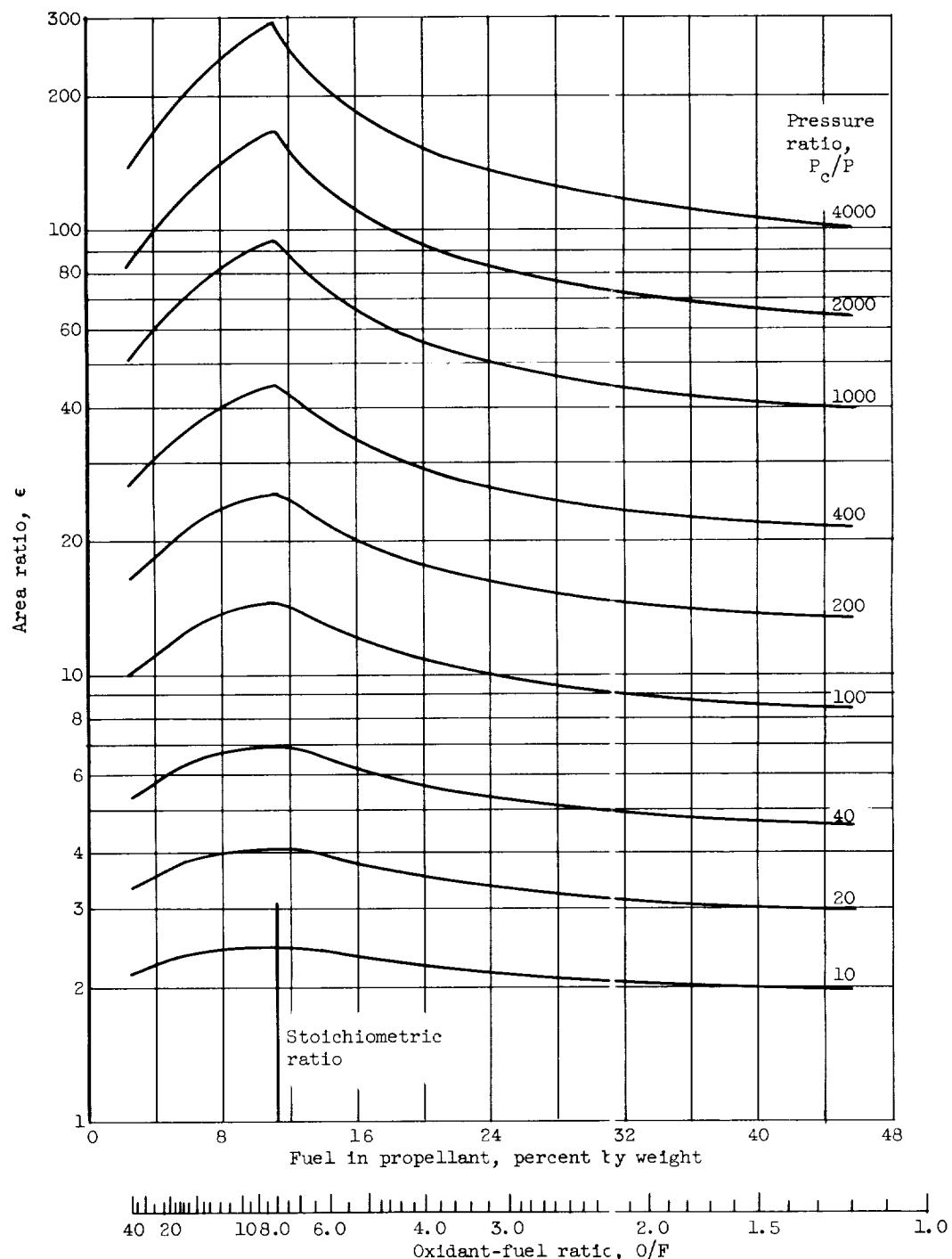
(d) Chamber pressure, 150 pounds per square inch absolute; equilibrium composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



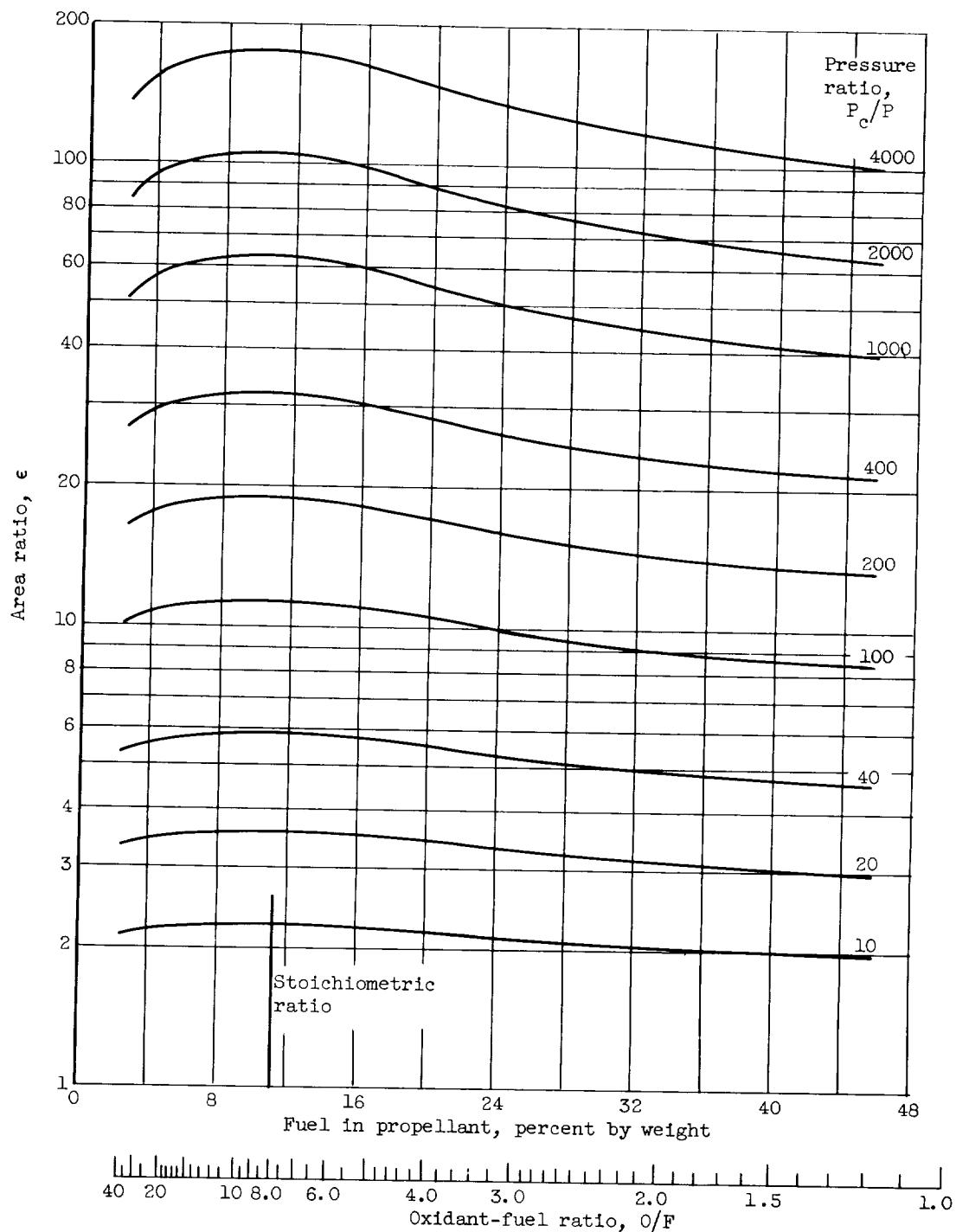
(e) Chamber pressure, 300 pounds per square inch absolute; frozen composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



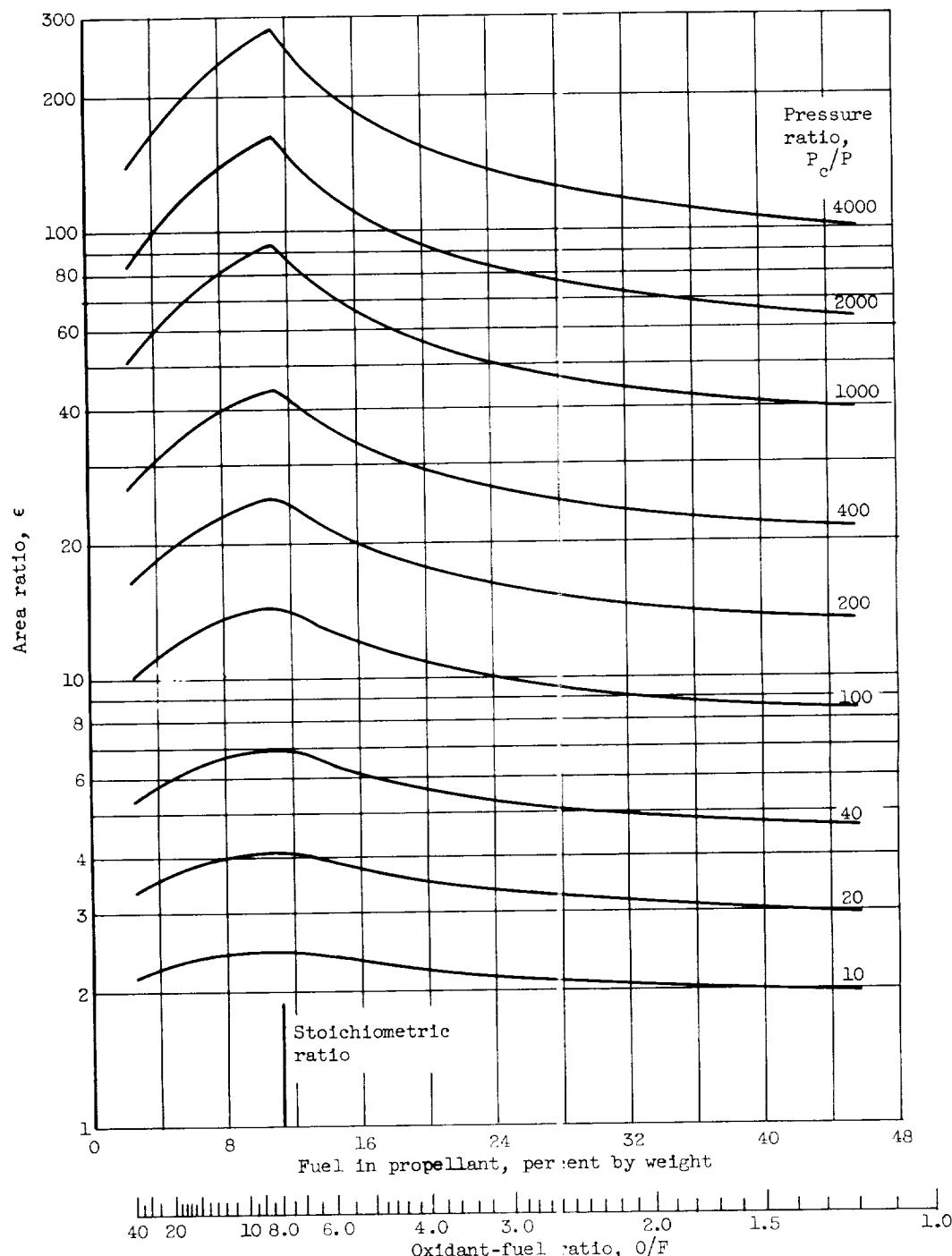
(f) Chamber pressure, 300 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



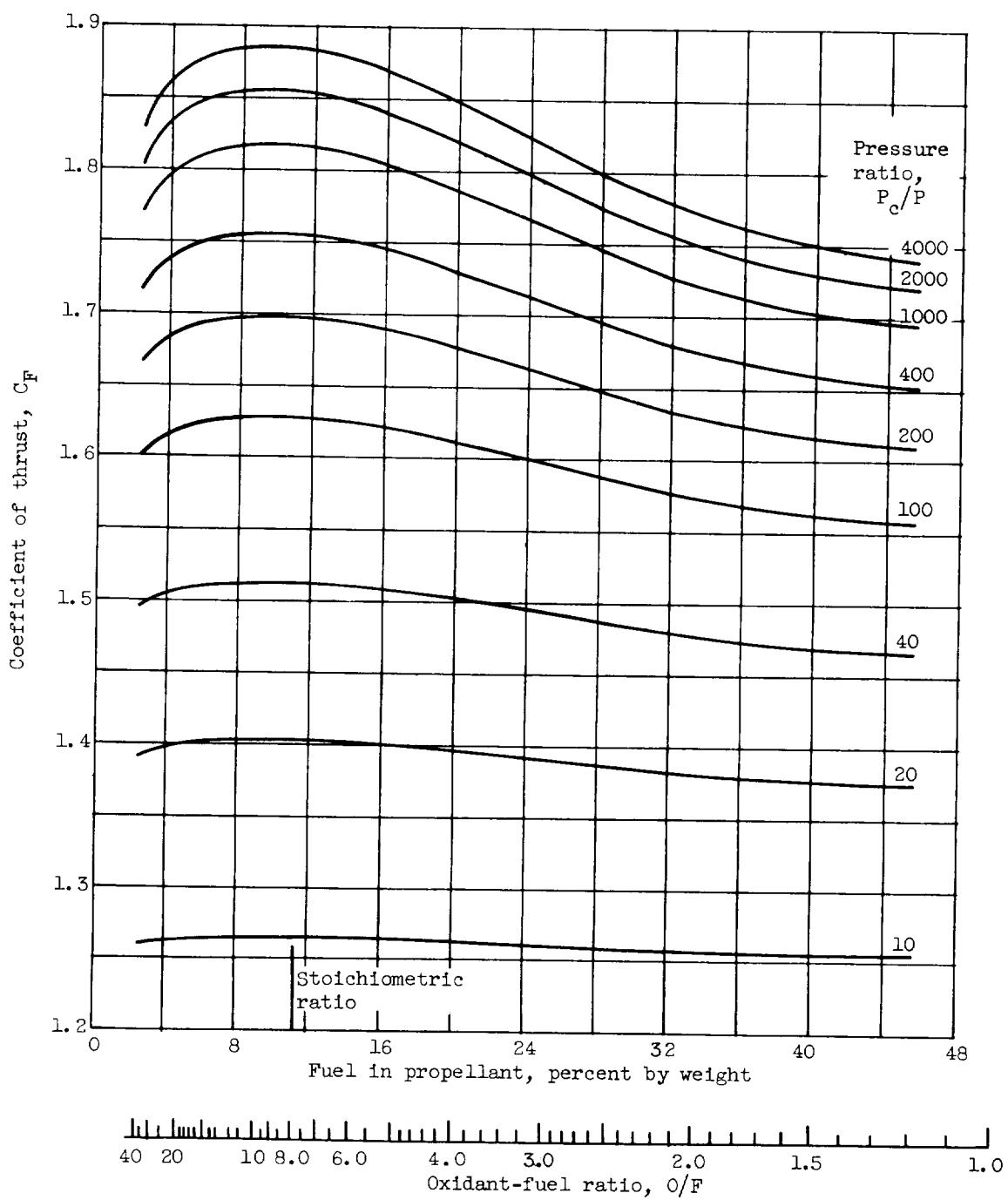
(g) Chamber pressure, 600 pounds per square inch absolute;
frozen composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



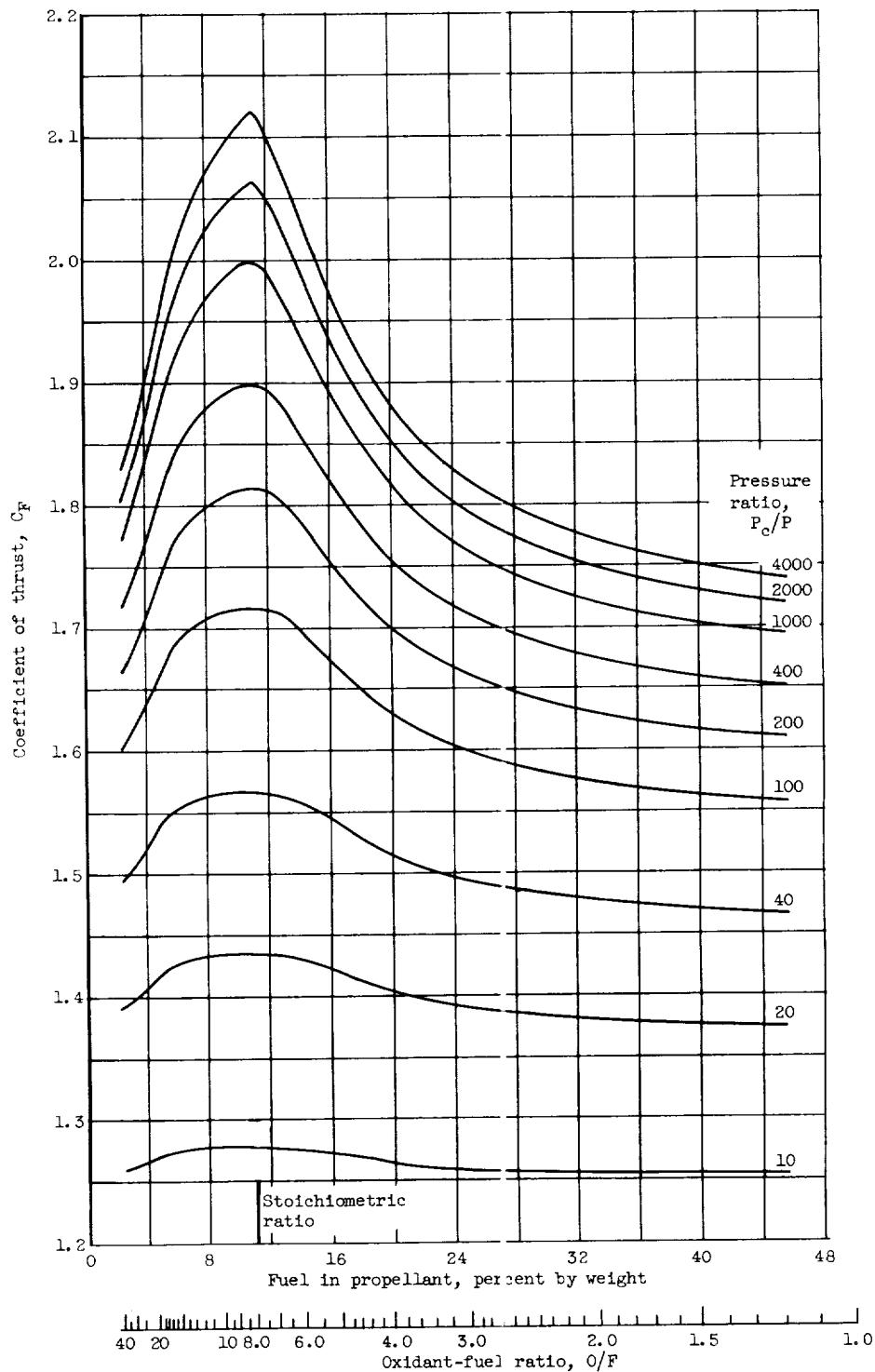
(b) Chamber pressure, 600 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 3. - Concluded. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



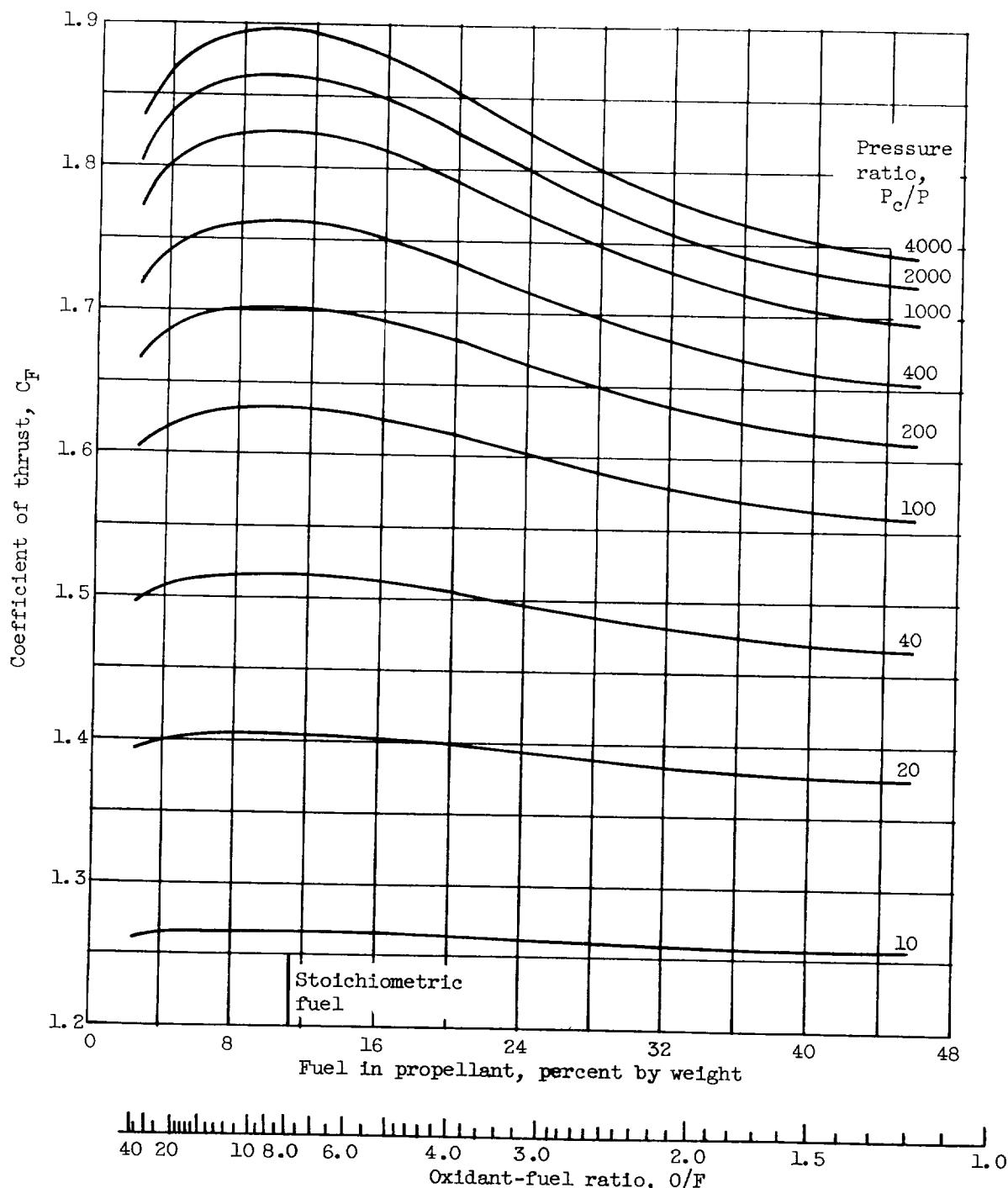
(a) Chamber pressure, 60 pounds per square inch absolute; frozen composition during expansion.

Figure 4. - Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



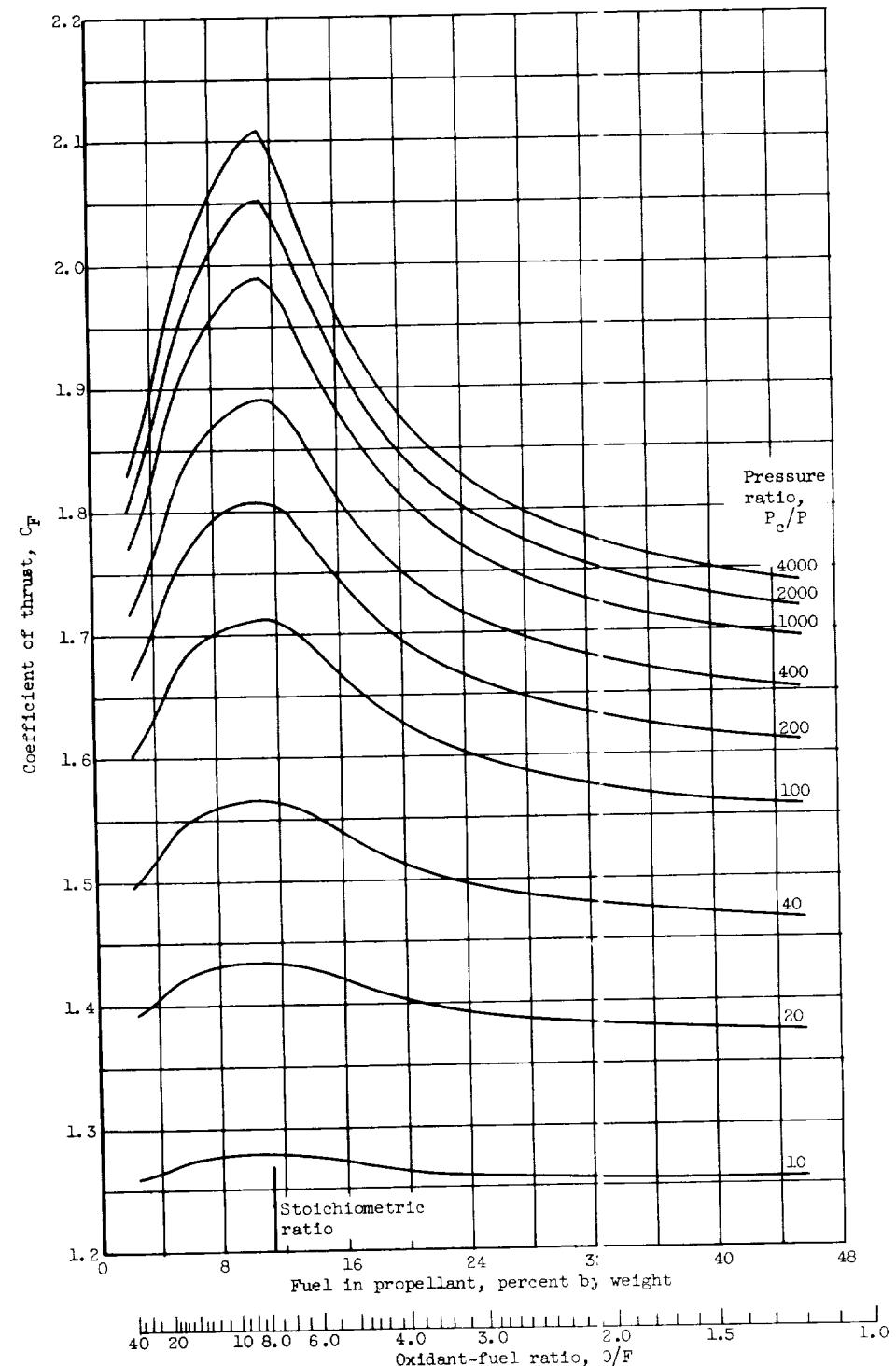
(b) Chamber pressure, 60 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



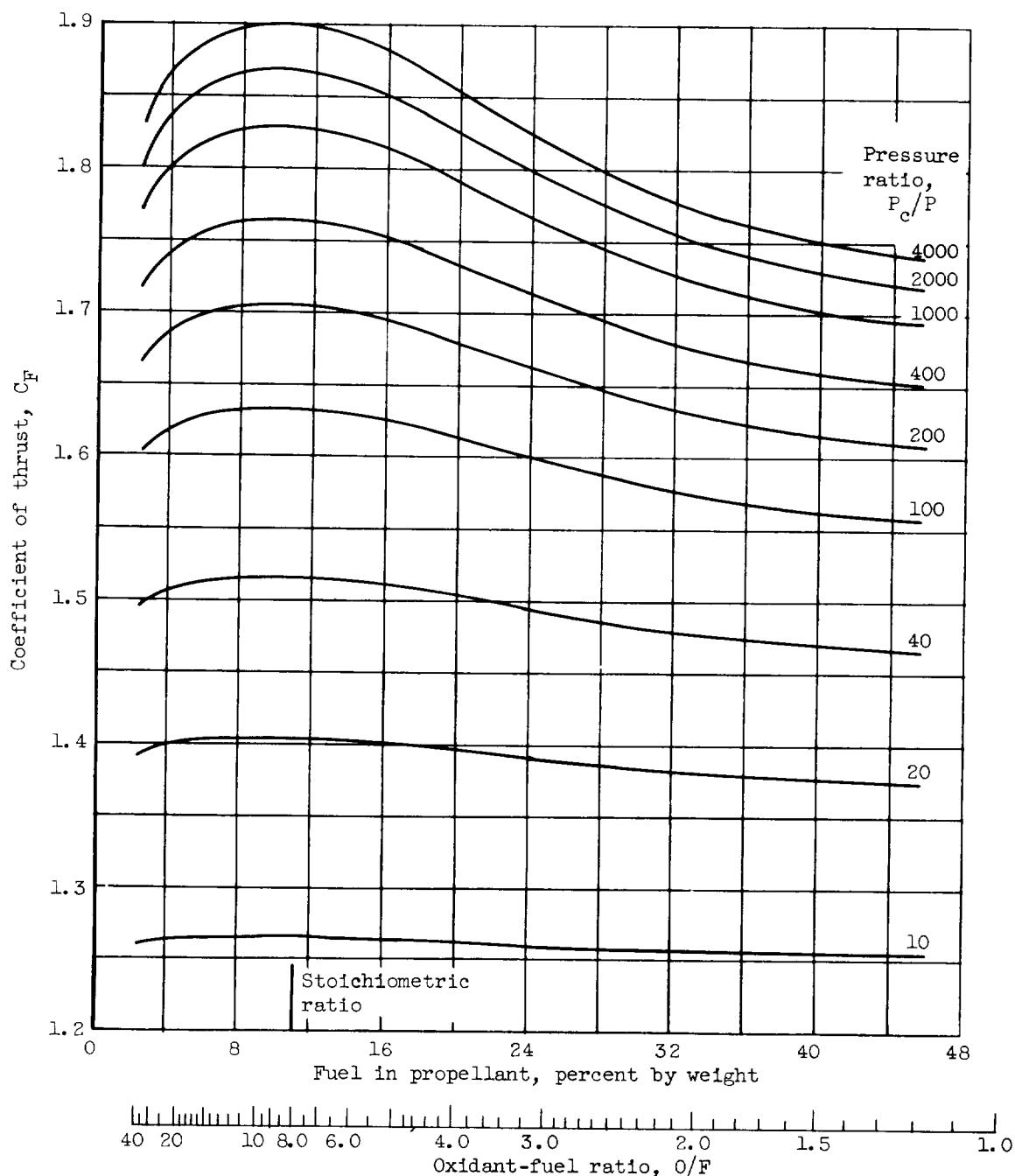
(c) Chamber pressure, 150 pounds per square inch absolute;
frozen composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



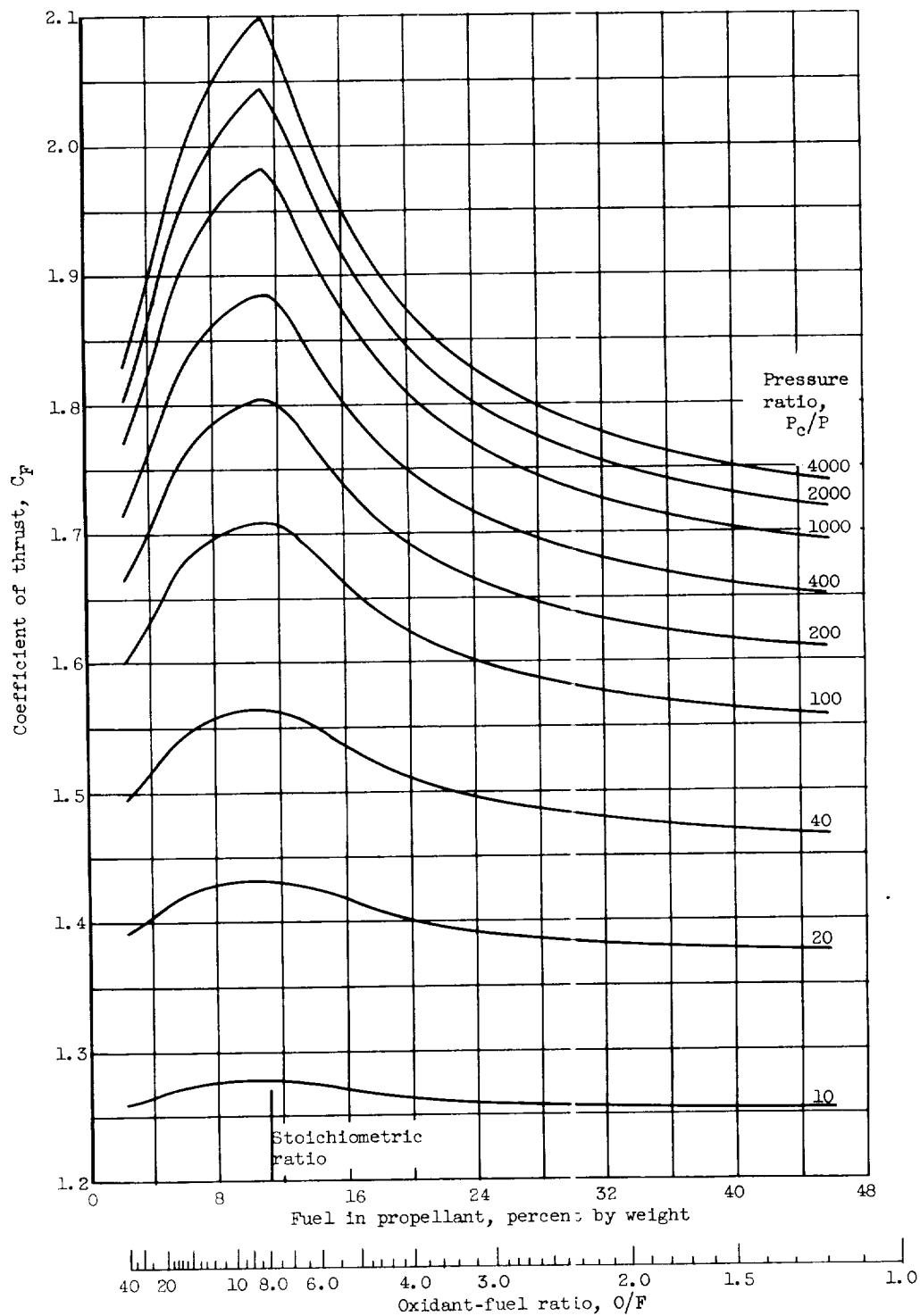
(d) Chamber pressure, 150 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen
and liquid oxygen. Isentropic expansion to pressure ratio indicated.



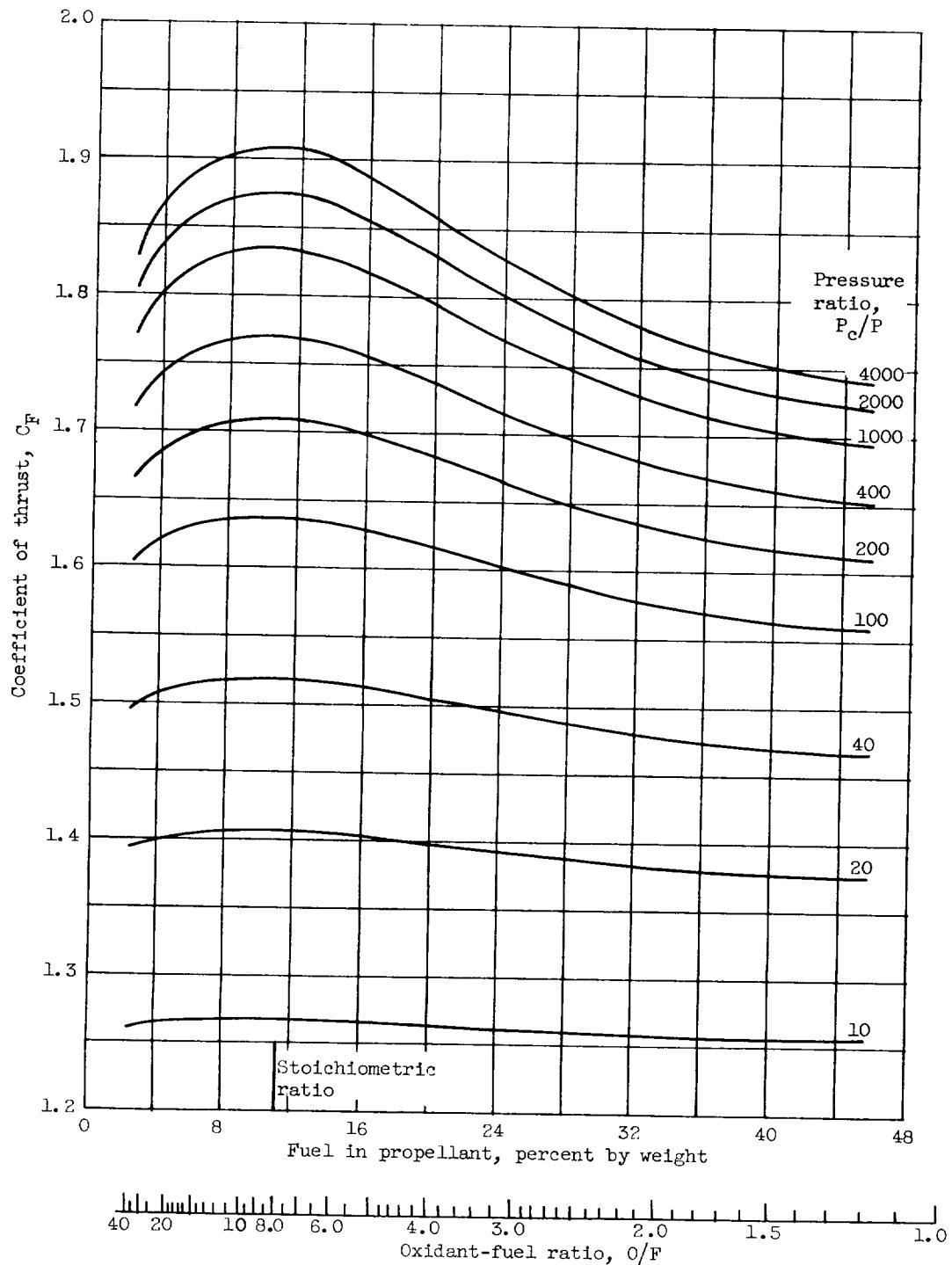
(e) Chamber pressure, 300 pounds per square inch absolute;
frozen composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



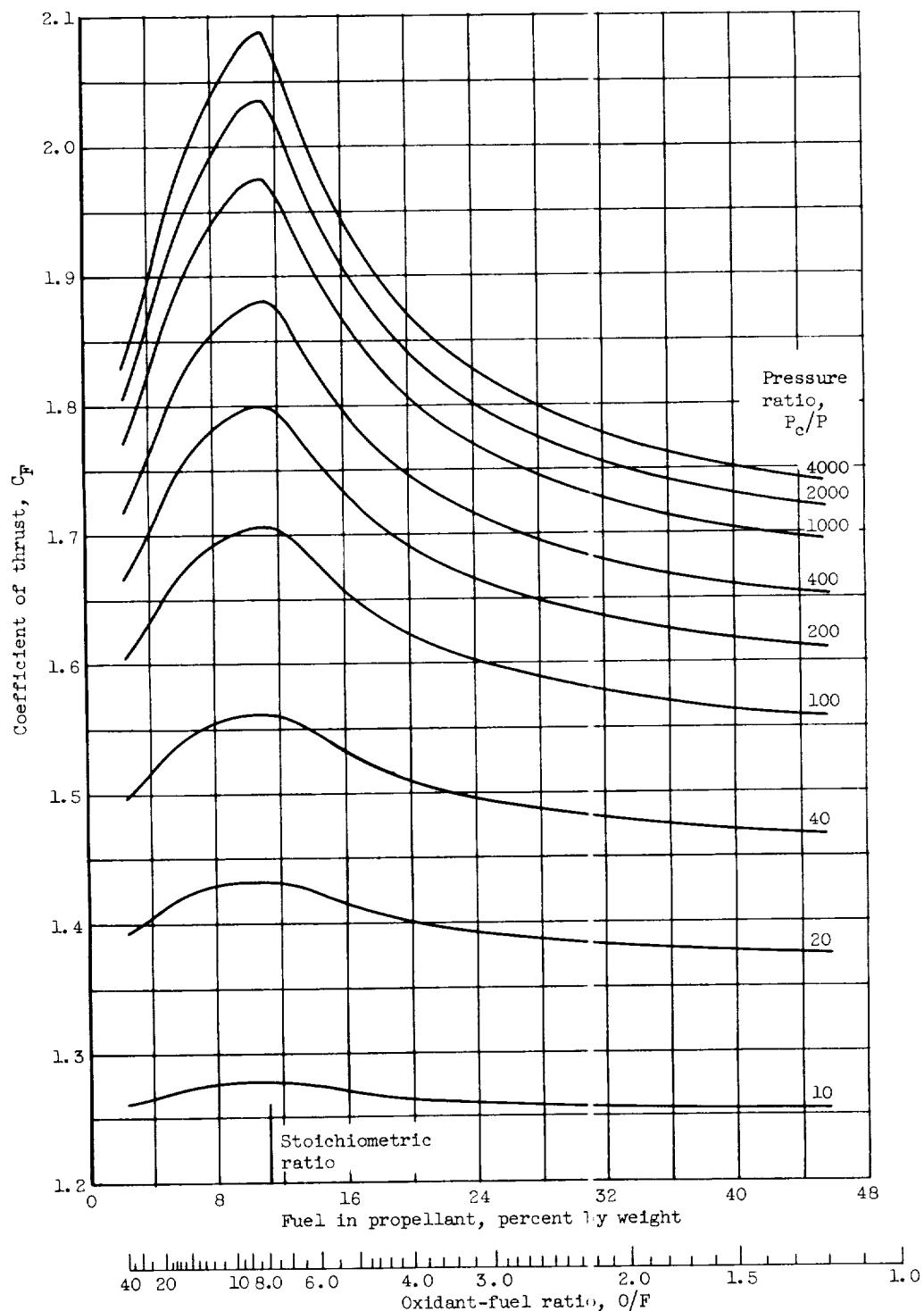
(f) Chamber pressure, 300 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen
and liquid oxygen. Isentropic expansion to pressure ratio indicated.



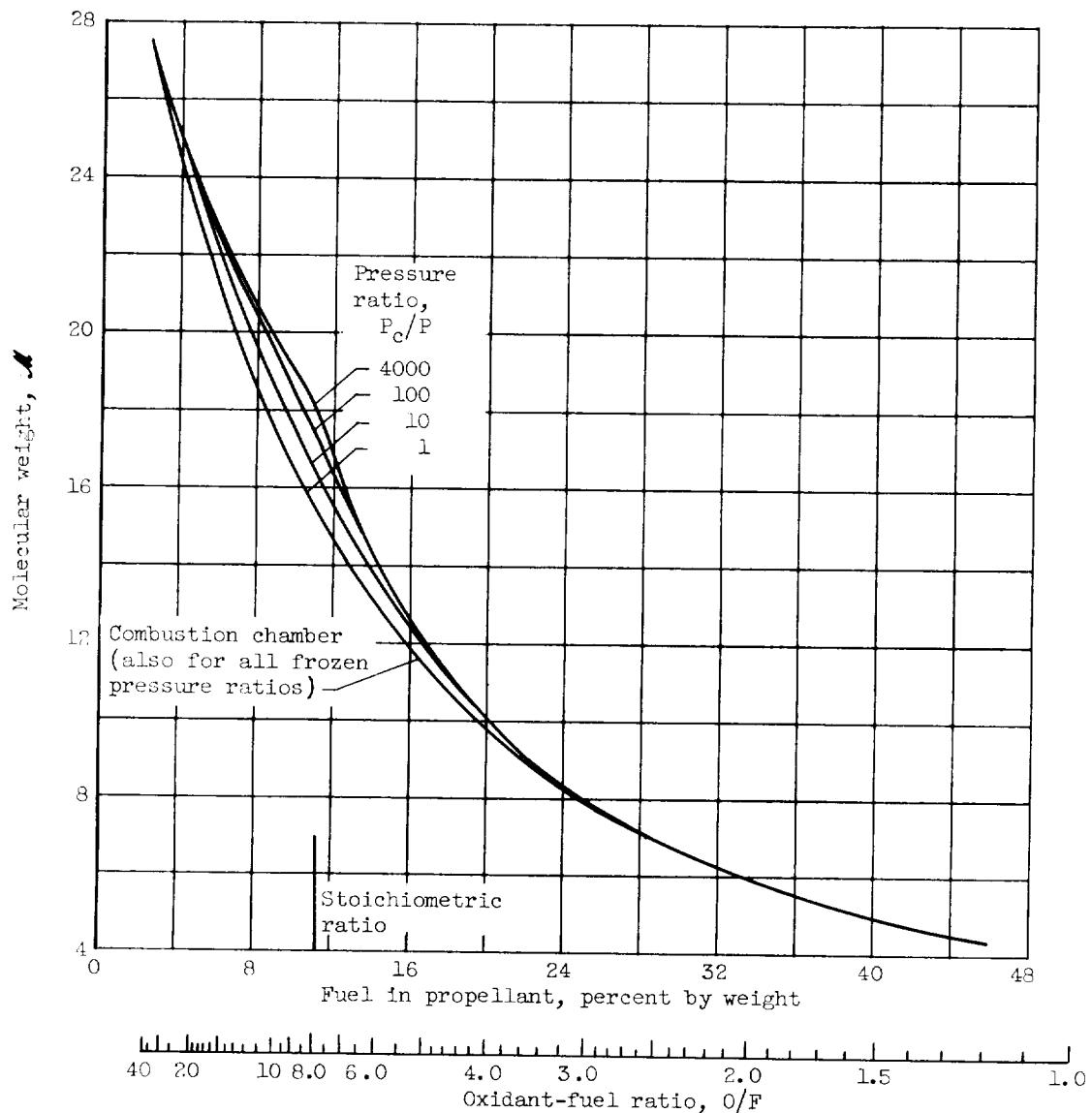
(g) Chamber pressure, 600 pounds per square inch absolute; frozen composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



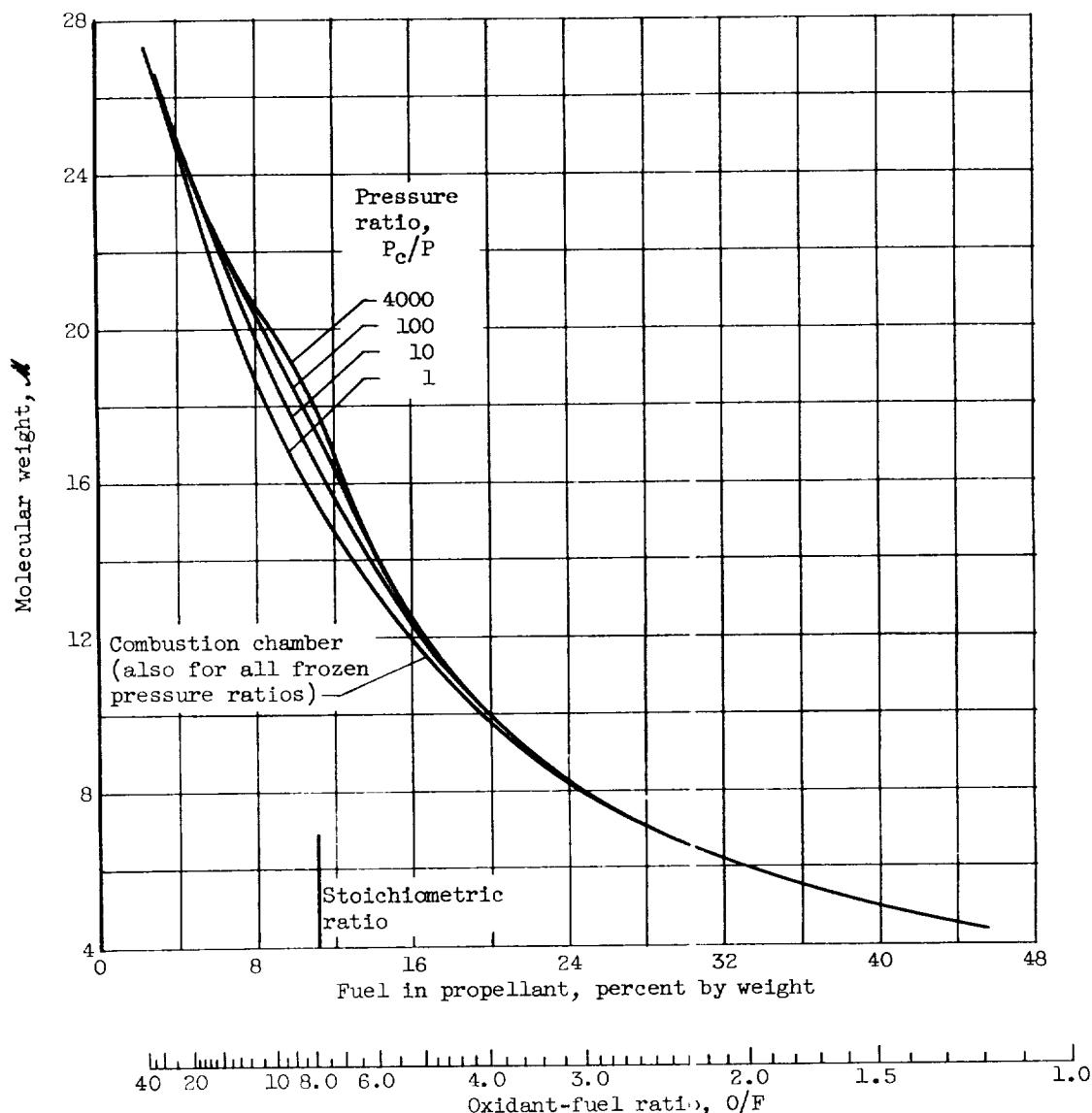
(h) Chamber pressure, 600 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 4. - Concluded. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



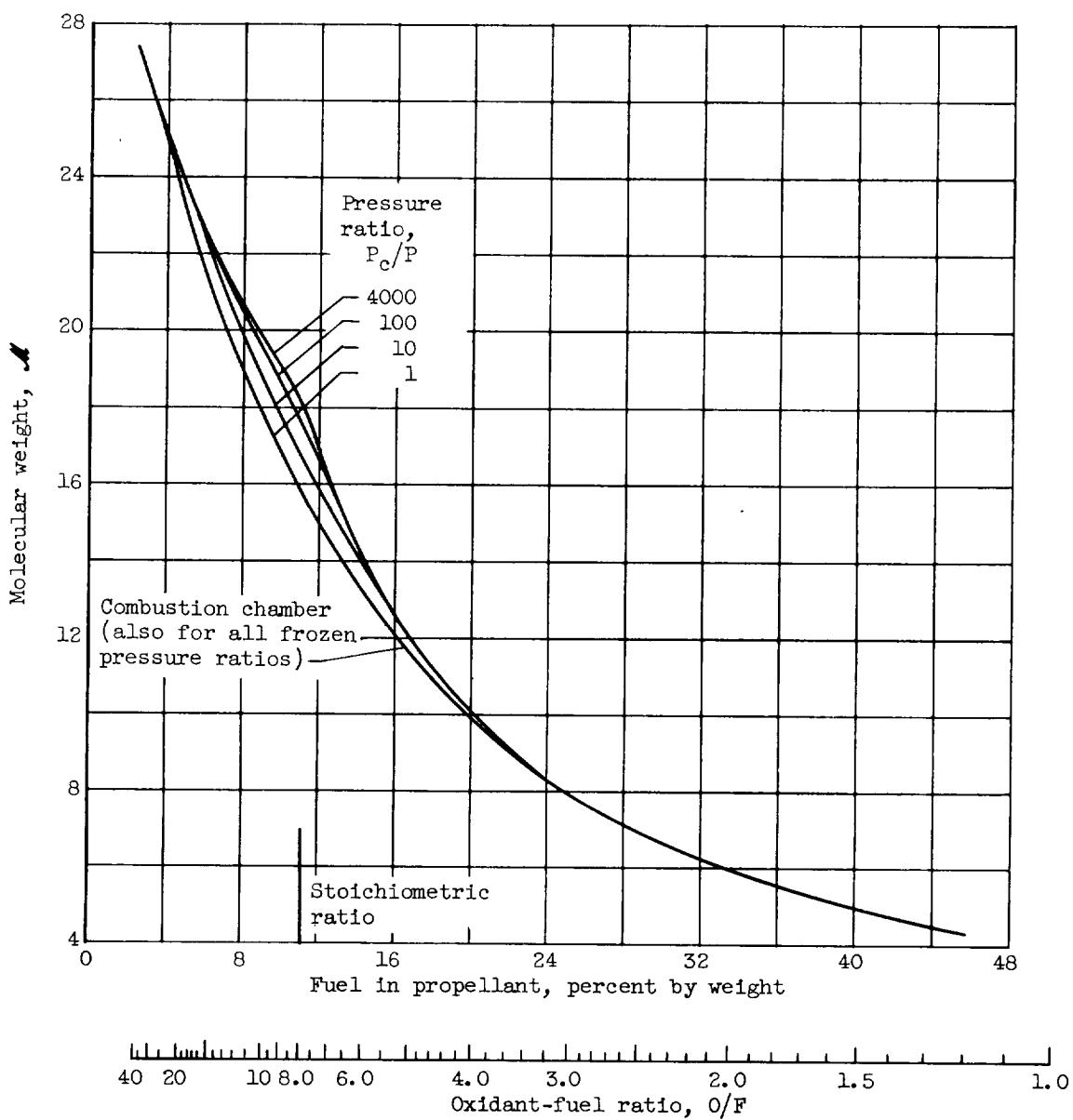
(a) Chamber pressure, 60 pounds per square inch absolute.

Figure 5. - Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



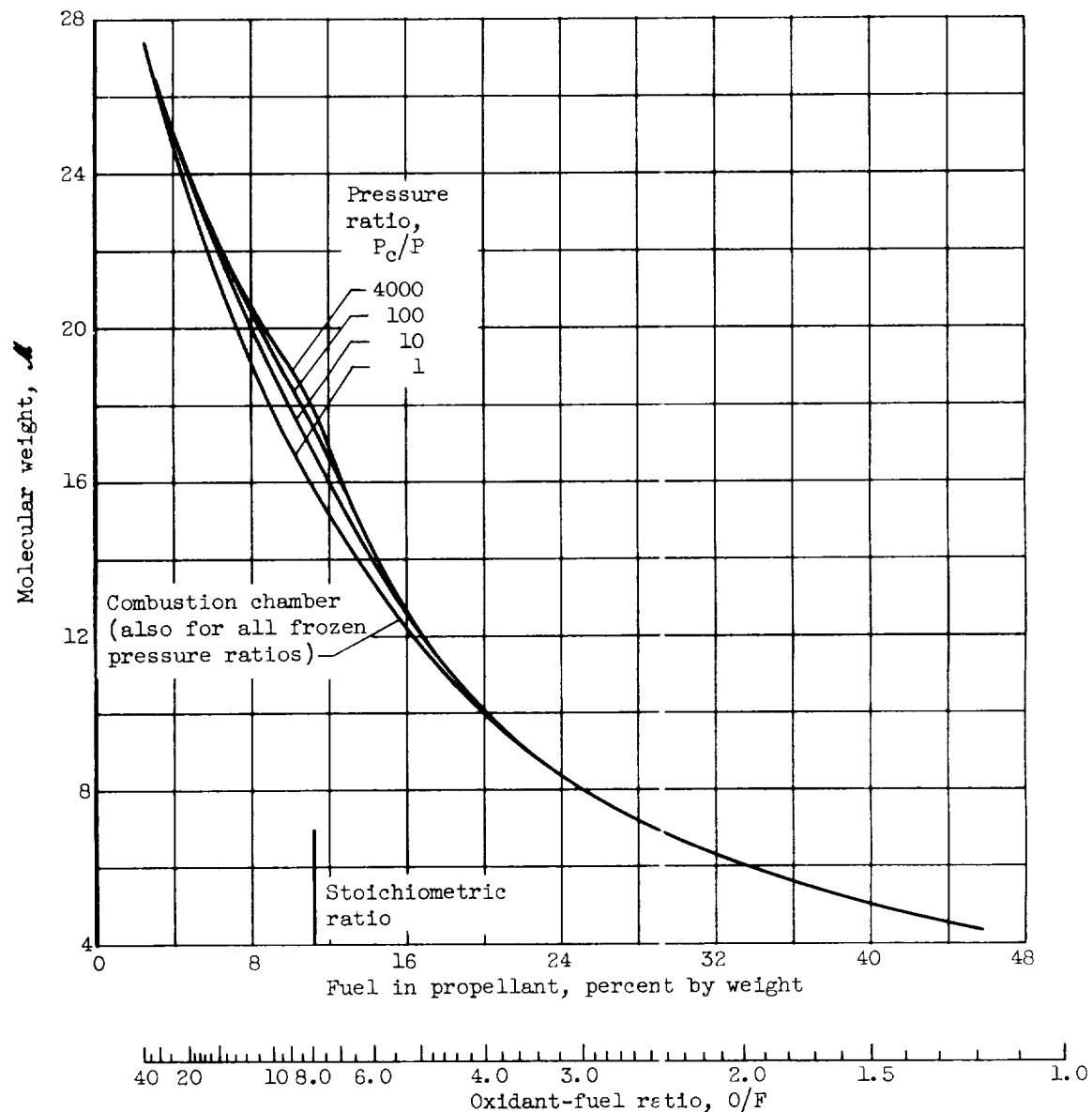
(b) Chamber pressure, 150 pounds per square inch absolute.

Figure 5. - Continued. Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



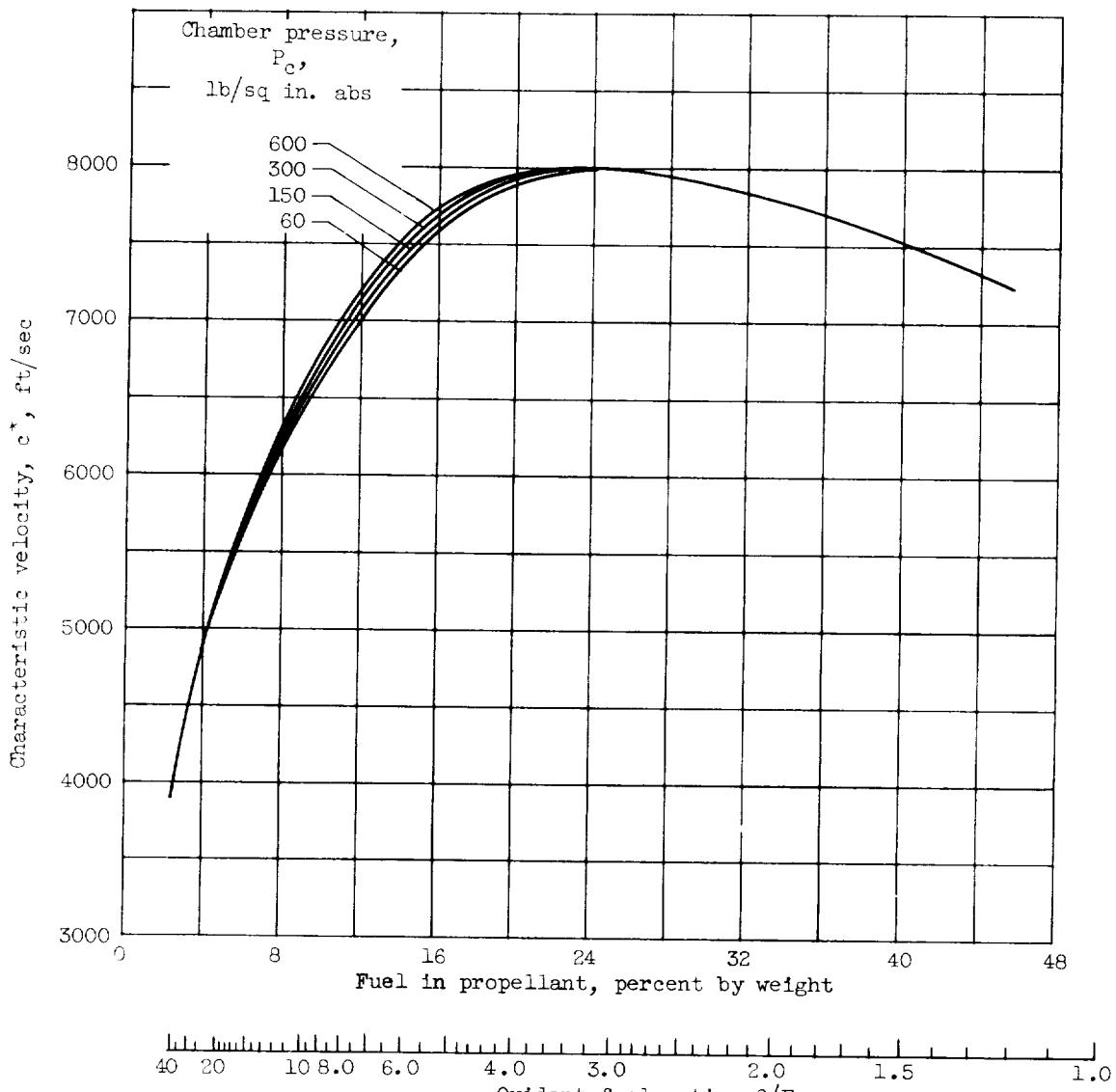
(c) Chamber pressure, 300 pounds per square inch absolute.

Figure 5. - Continued. Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



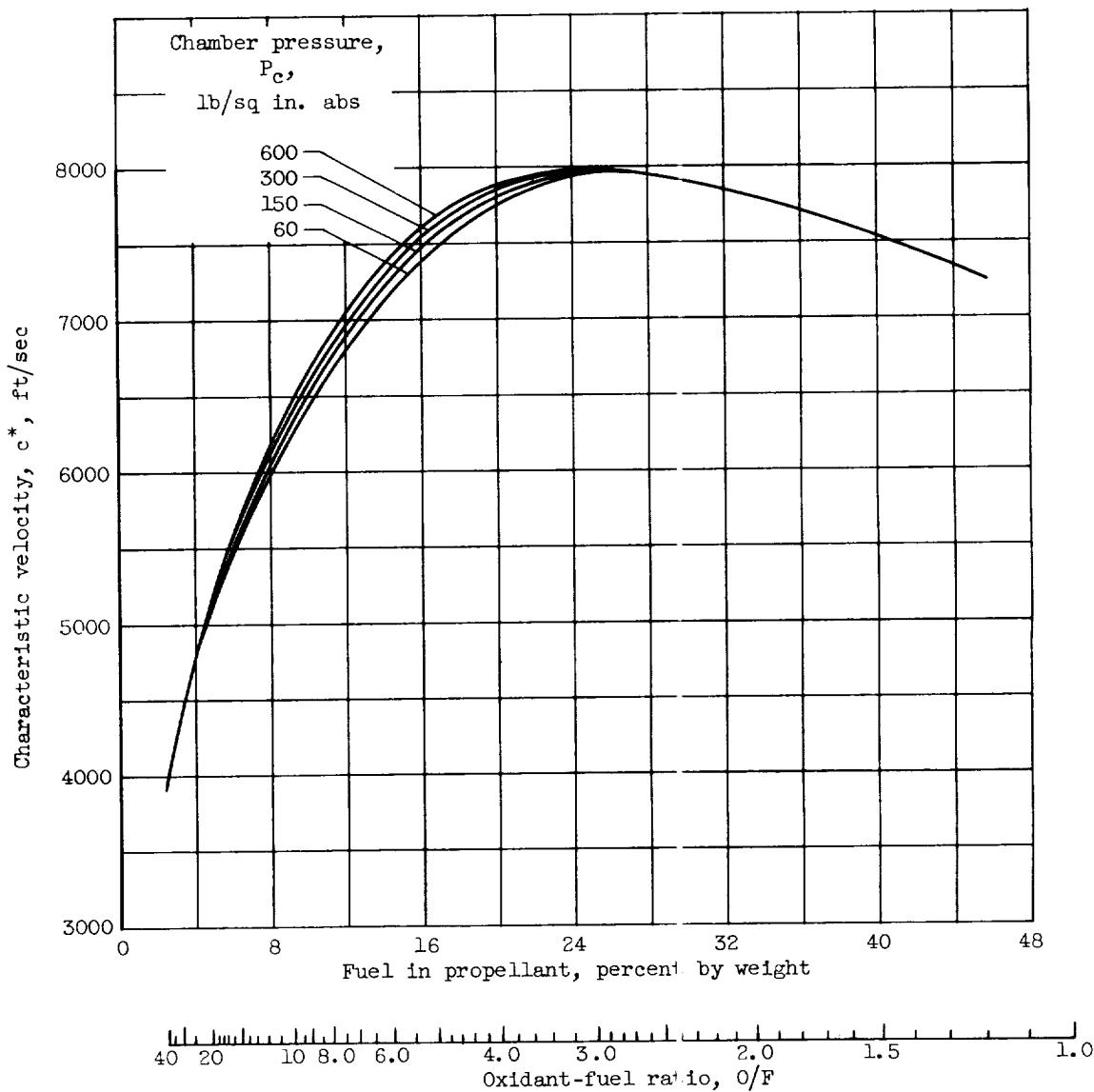
(d) Chamber pressure, 600 pounds per square inch absolute.

Figure 5. - Concluded. Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



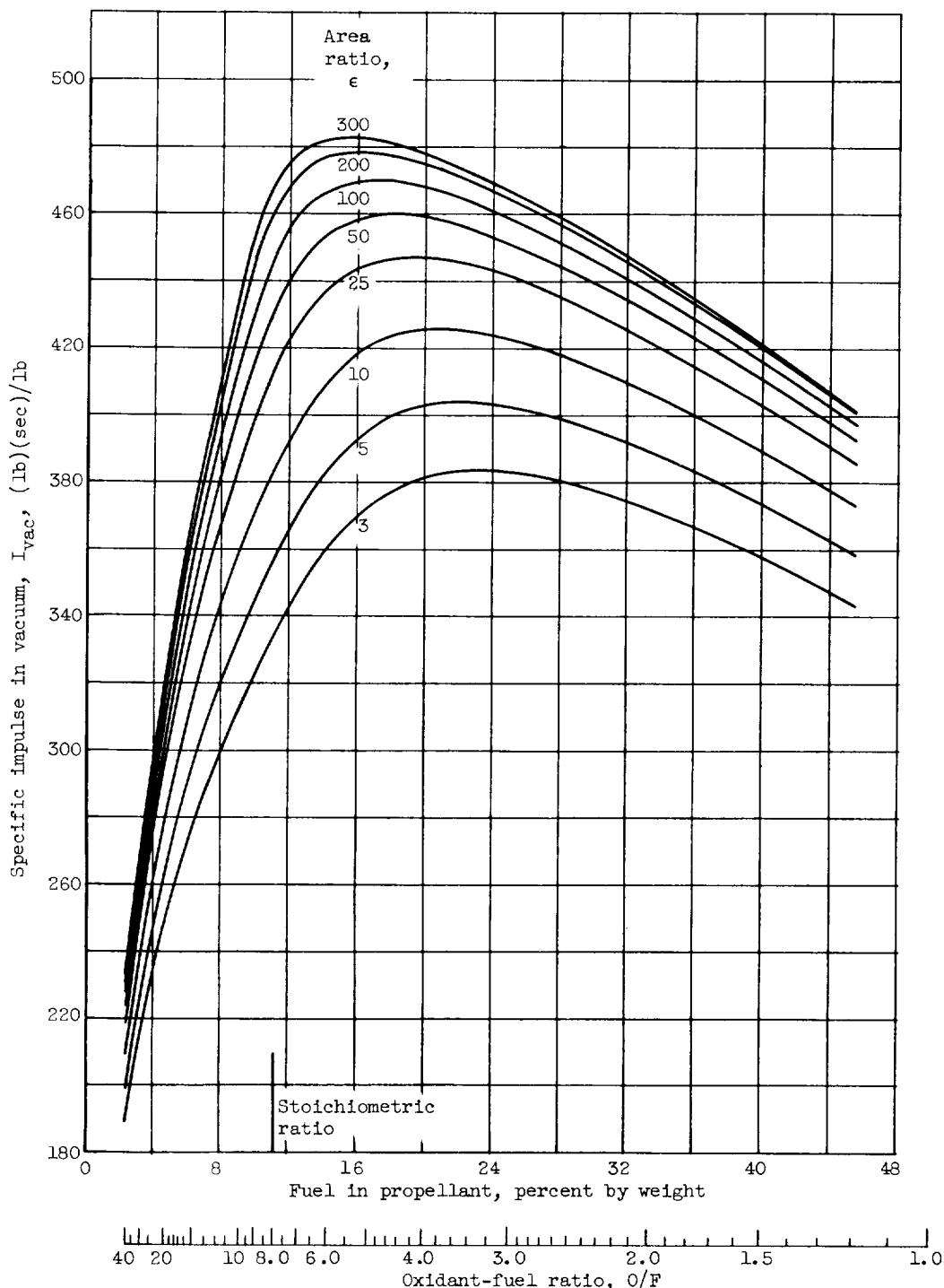
(a) Equilibrium composition during expansion.

Figure 6. - Theoretical characteristic velocity of liquid hydrogen and liquid oxygen.



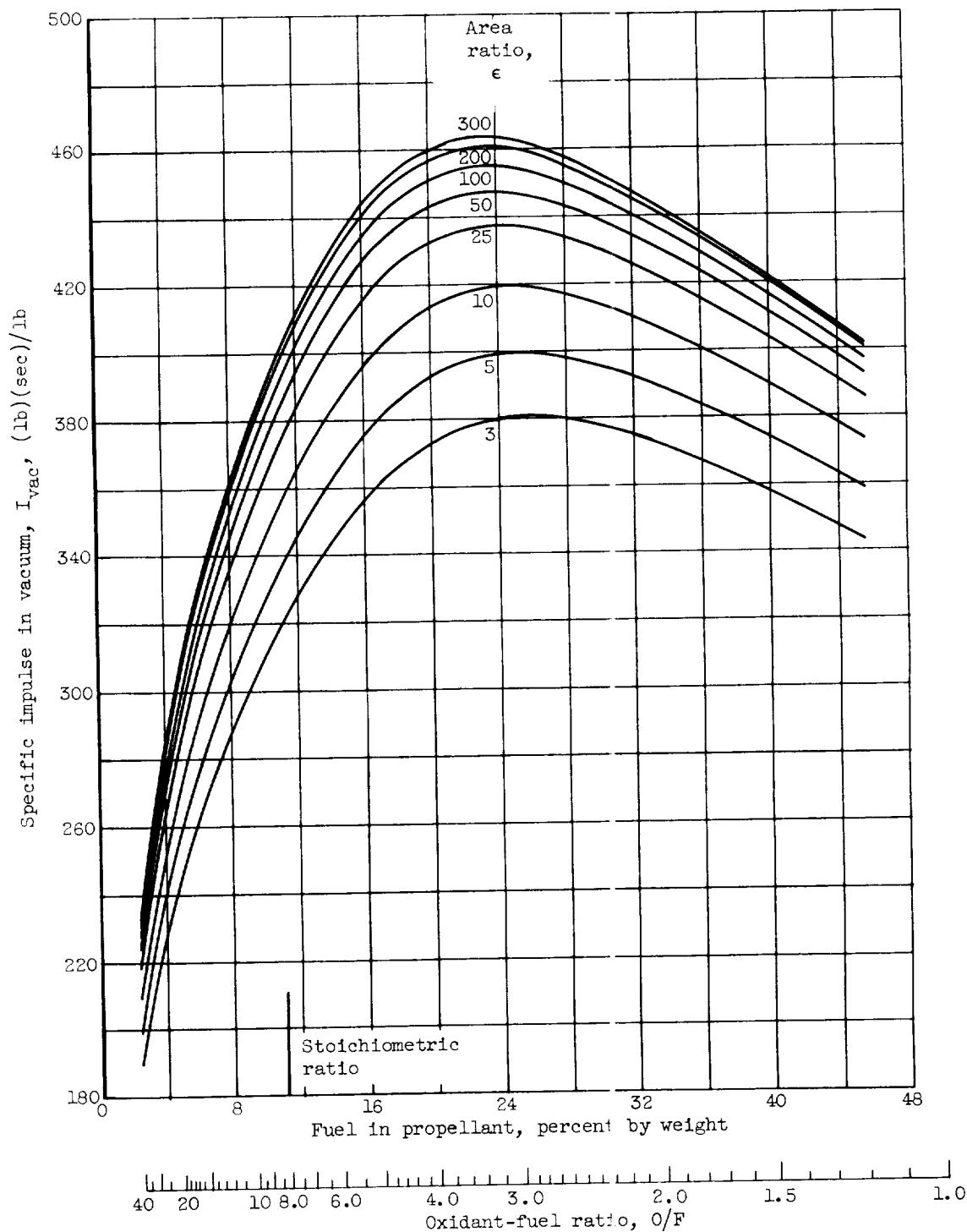
(b) Frozen composition during expansion.

Figure 6. - Concluded. Theoretical characteristic velocity of liquid hydrogen and liquid oxygen.



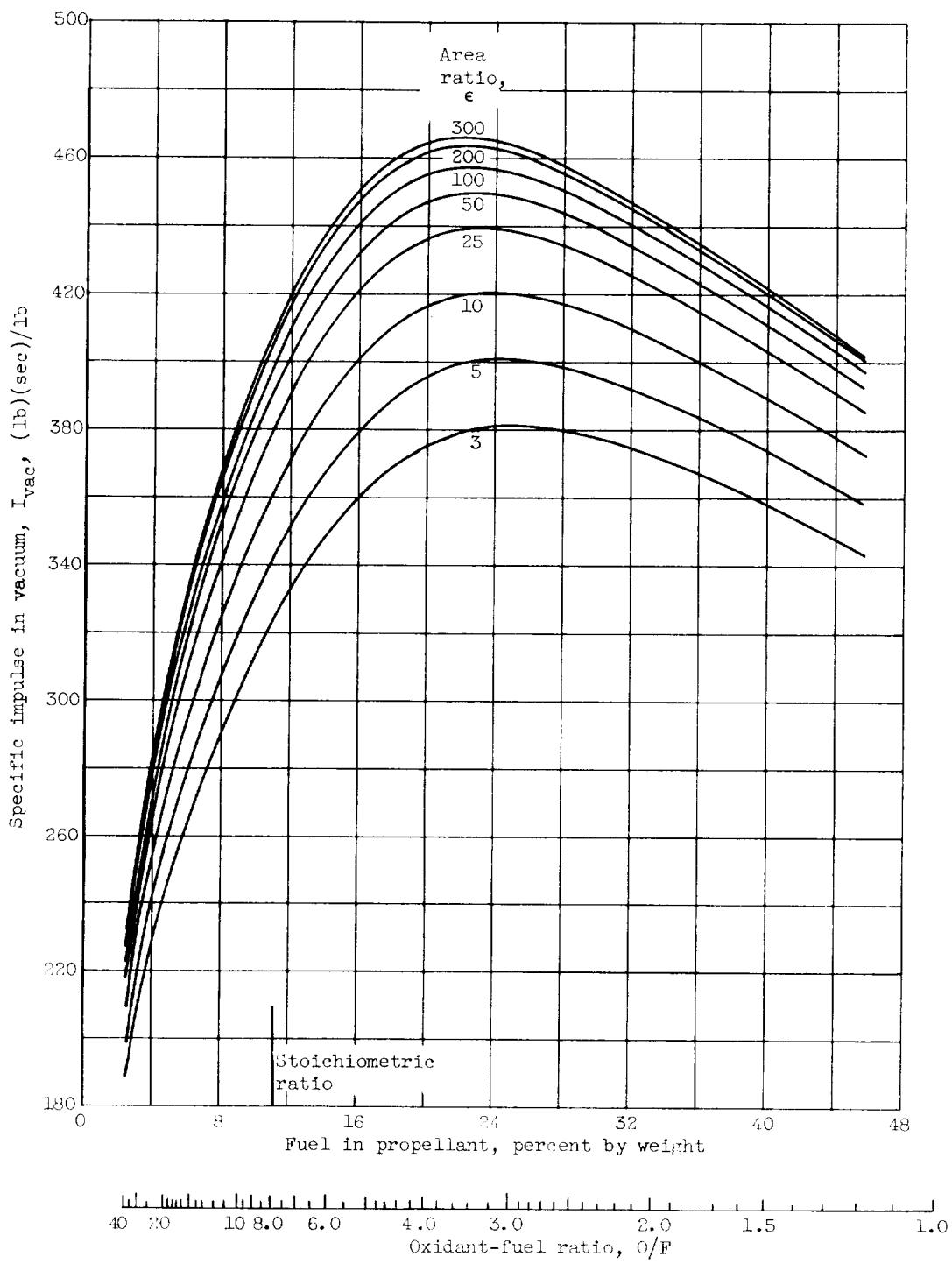
(b) Chamber pressure, 60 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



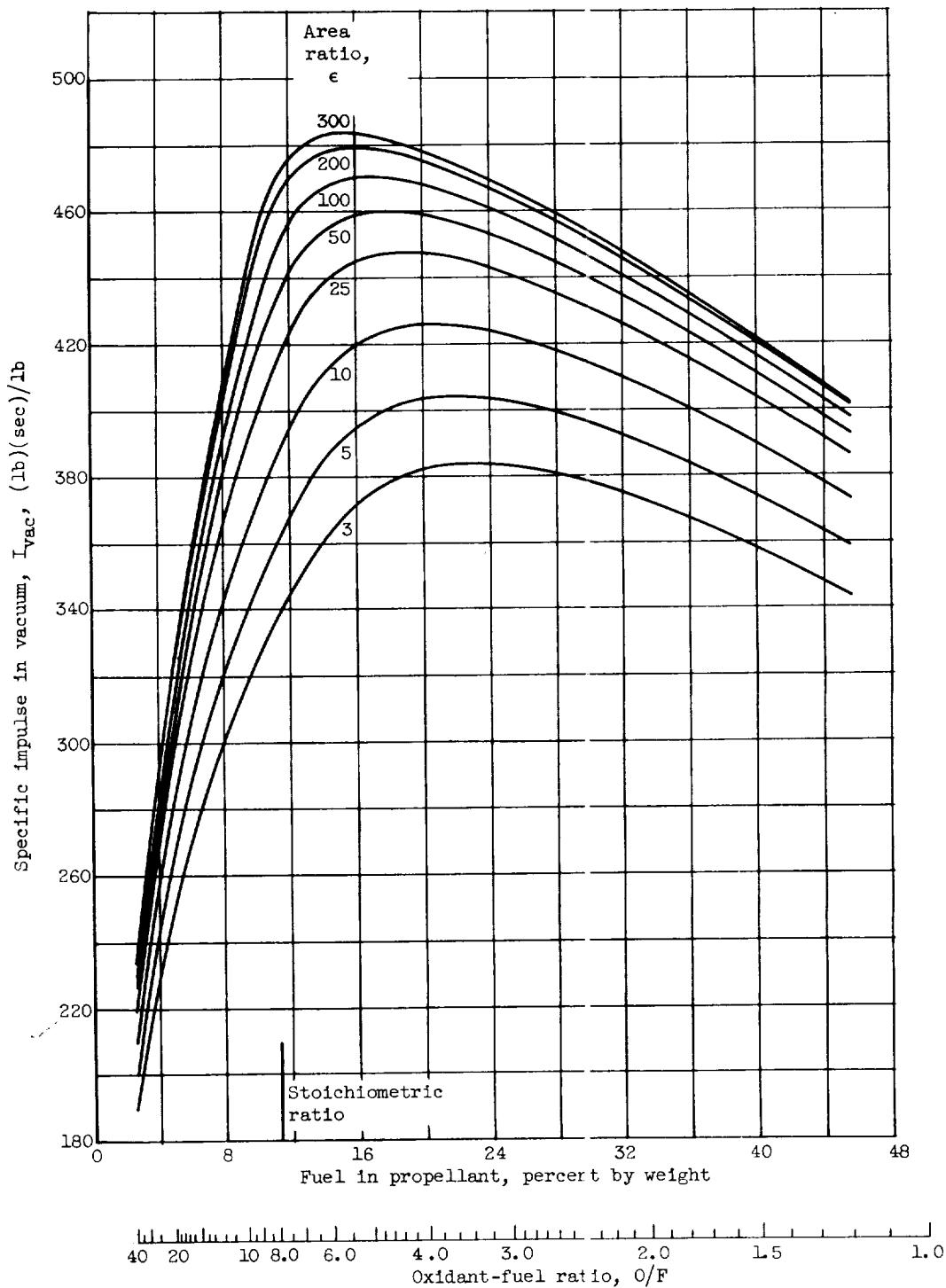
(a) Chamber pressure, 60 pounds per square inch absolute;
frozen composition during expansion.

Figure 7. - Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



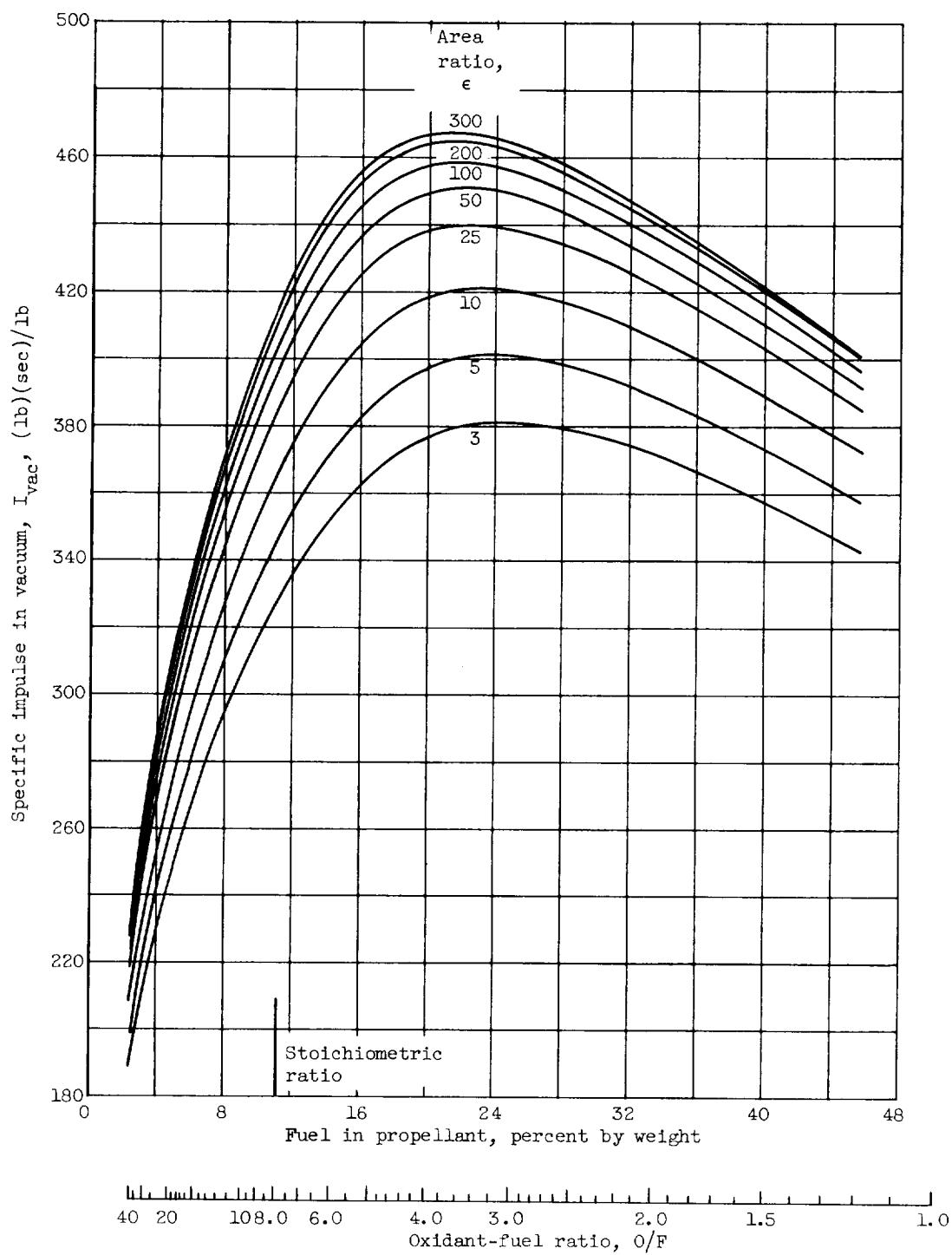
(c) Chamber pressure, 150 pounds per square inch absolute; frozen composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



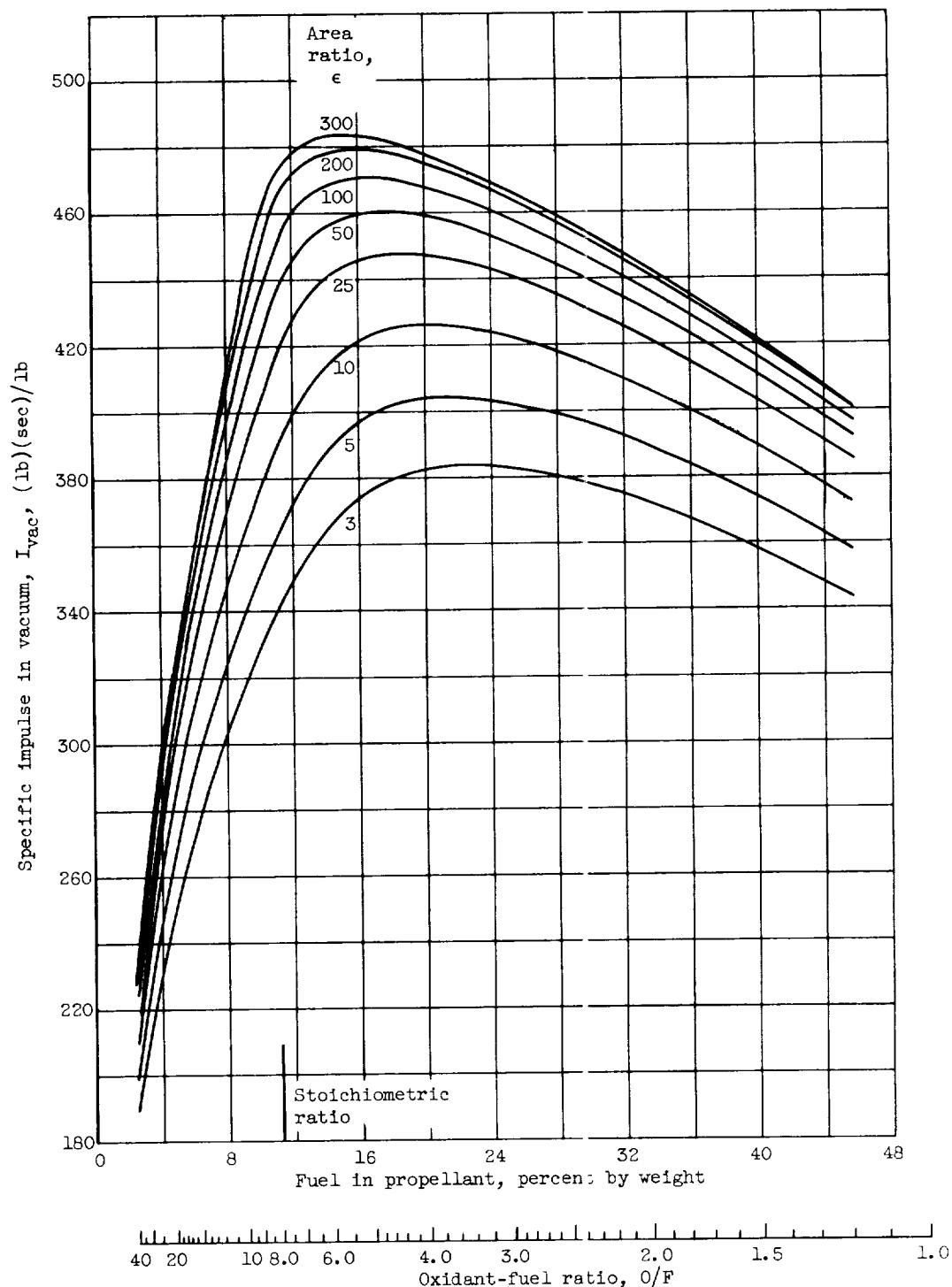
(d) Chamber pressure, 150 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



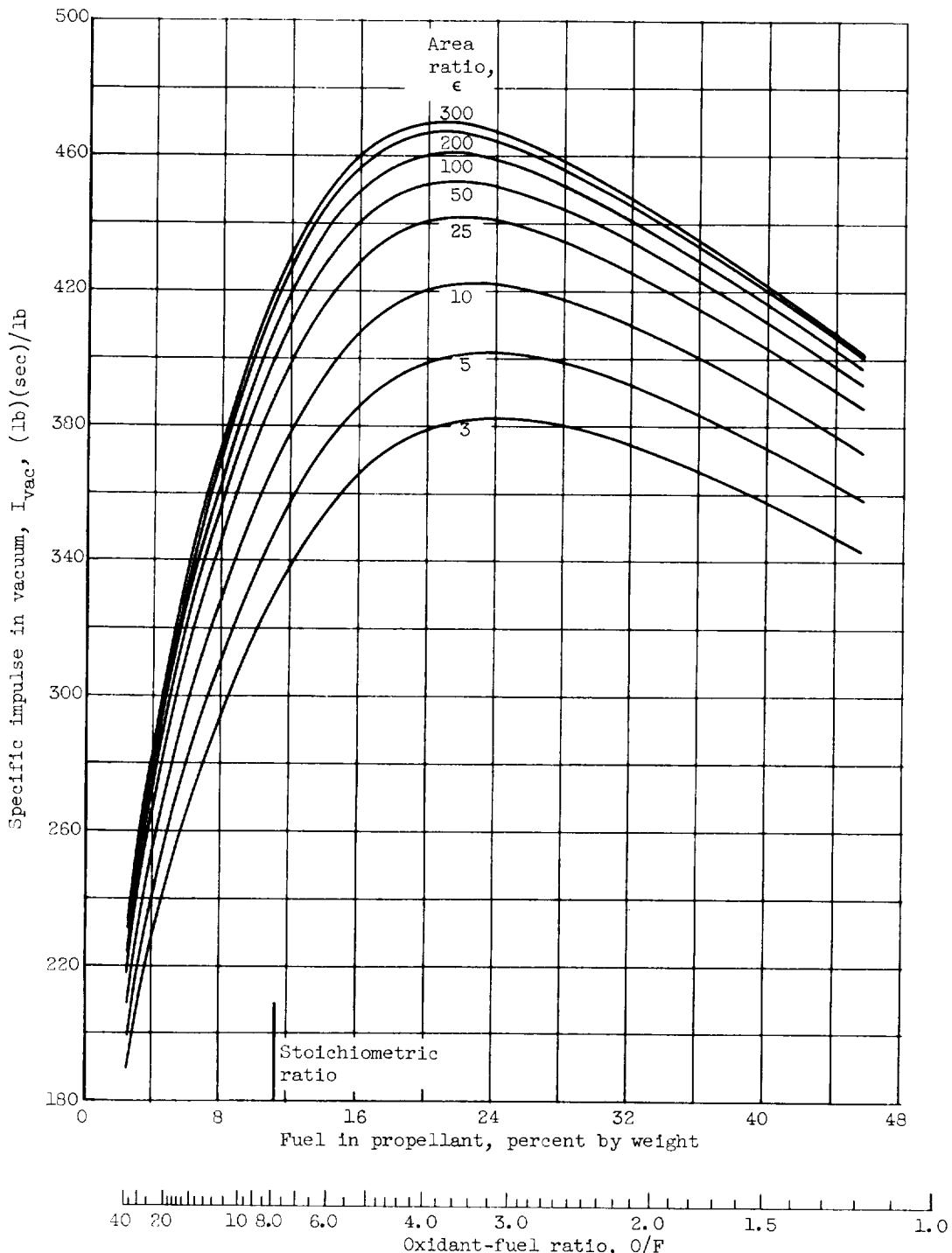
(e) Chamber pressure, 300 pounds per square inch absolute;
frozen composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



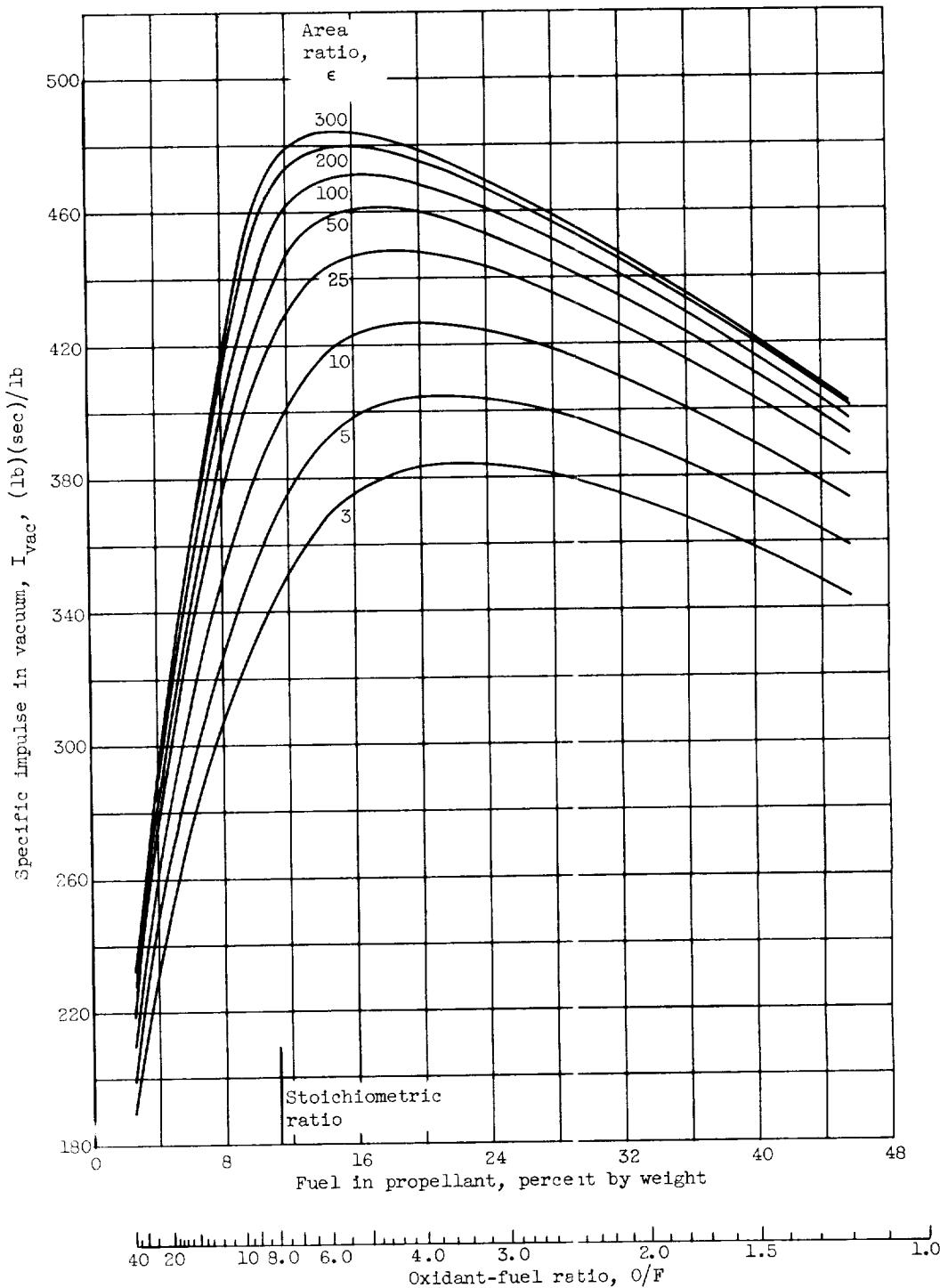
(f) Chamber pressure, 300 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



(g) Chamber pressure, 600 pounds per square inch absolute; frozen composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



(h) Chamber pressure, 600 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 7. - Concluded. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.

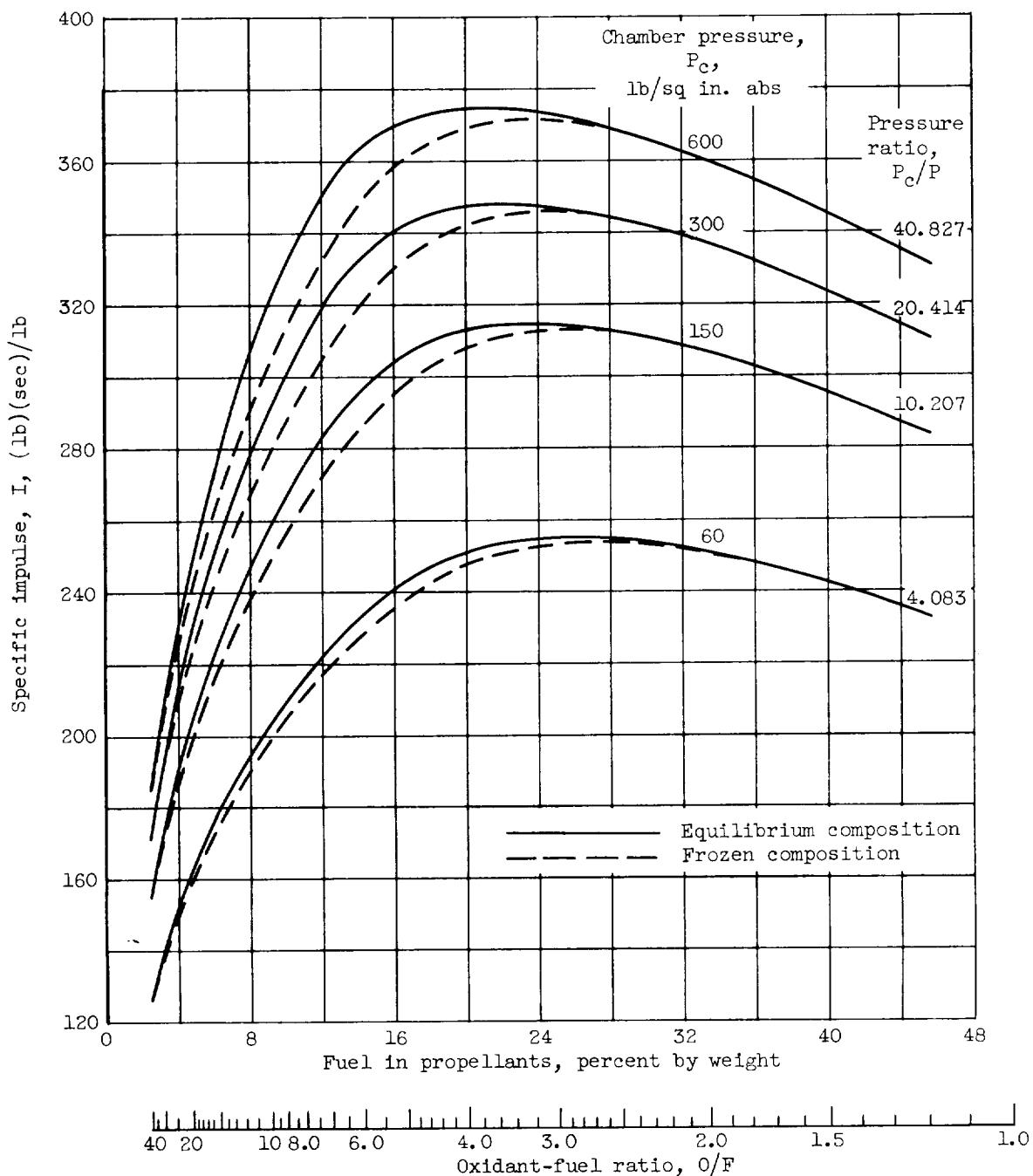


Figure 8. - Theoretical specific impulse for liquid hydrogen with liquid oxygen. Isentropic expansion to 1 atmosphere from chamber pressure indicated.

