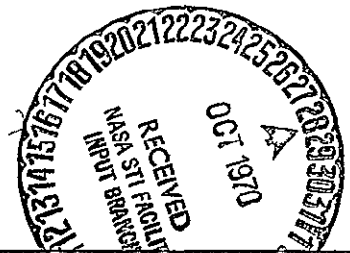
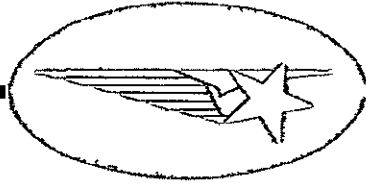


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SCALING PARAMETERS FOR THE
SIMULATION OF HIGHLY EXPANDED
ROCKET EXHAUST PLUMES AND
THE RESULTANT IMPINGEMENT
FORCES ON AN IMMERSED BODY


July 1970

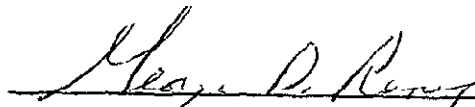
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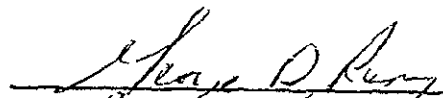
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FOREWORD

This document presents results of work performed by Lockheed Missiles and Space Company, Huntsville Research and Engineering Center under Contract NAS8-24437, Scaling Parameters/Low Density Plume Impingement Force Data, to the Aero-Astroynamics Laboratory of NASA/Marshall Space Flight Center. The Technical monitor was Mr. V. K. Henson of the Aero-Astroynamics Laboratory.

SUMMARY

Literature dealing with the proper scaling of rocket exhaust plumes with nonreacting gas mixtures is reviewed. From this background, a technique was developed to select gases which will properly simulate a region of a prototype plume, and the technique is outlined. A gas simulant selection computer program is then presented and discussed. The computer program performs the gas simulant selection based upon the parameter desired to approximate, i.e., impingement forces, Mach number, or Reynolds number. Results of this program for two typical engines are discussed.

A specific parameter of a region of a prototype plume can, in general, be simulated. In particular, the momentum flux of a plume appears to be rather easily duplicated for a definite region of a plume. Typical selections resulted in about a three percent error in momentum flux. This result lends credence to the goal of simulating experimentally the impingement forces of high altitude plumes on orbital bodies.

In addition, the Mach number may possibly be simulated by adjusting gas composition and chamber temperature. (These results are based on the possibility of simulating the condensation phenomena.) This simulation does appear to be feasible if the chamber properties can be varied enough to match the point of vapor saturation in the flow field.

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NOMENCLATURE

Symbol

| | |
|-------|--|
| a | speed of sound |
| A | area |
| C_v | specific heat at constant volume |
| C_p | specific heat at constant pressure |
| D | diameter dimension |
| E | constant defined by equation of text |
| f_1 | scale factor for the 1 th parameter |
| F | force |
| g | number of molecules per drop |
| G | generalized function |
| h | specific enthalpy |
| H | enthalpy |
| J | drop formation rate |
| k | Boltzmann's constant |
| Kn | Knudsen number |
| l | representative length |
| m | mass of molecular of vapor |
| m | mass flux of gas |
| M | Mach number |
| n | weight fraction |
| N | constant defined by equations of text |

| | |
|-------|---|
| N_g | fractional condensation rate |
| P | pressure |
| Pr | Prandtl number |
| r | radius |
| s | radial distance from exit plane of nozzle |
| SF | geometric scale factor |
| T | temperature |
| v | velocity |
| V | volume of drop |
| X | axial direction |

Greek

| | |
|-----------|-------------------------------------|
| α | Knudsen number correction factor |
| β | momentum correction factor |
| γ | specific heat ratio |
| δ | boundary layer thickness |
| ζ | surface tension |
| θ | flow angle |
| λ | molecular mean free path |
| μ | viscosity |
| ν | Prandtl-Meyer expansion angle |
| ρ | density of gas |
| σ | collision cross section of molecule |
| ϕ | nozzle lip angle |
| ψ | molecular weight of gas |

Subscripts

| | |
|--------------|--|
| a | ambient conditions |
| cont | continuum flow conditions |
| d | drop |
| e | exit plane |
| FM | free molecular flow conditions |
| liq | liquid |
| m | model |
| o | stagnation conditions |
| p | prototype |
| S_{∞} | stagnation condition for drop of infinite radius |
| t | throat conditions |

Superscript

| | |
|---|-------------------------------|
| * | denotes drop of critical size |
|---|-------------------------------|

INTRODUCTION

Orbiting vehicles of the Apollo Applications Program and other space programs are generally maneuvered by reaction control rocket engines. In many cases, interaction and impingement of the exhaust plumes on the parent vehicles create control thrust degradations in conjunction with undesirable reaction forces and moments. If these plume impingement effects are not defined, inadequate control systems may result. Since orbiting vehicle configurations are generally complex (including extensive external hardware such as solar power cells, communication antennas, etc.) theoretical procedures for predicting vehicle plume impingement forces are quite complicated. By analyzing properly simulated experimental investigations, impingement forces on complex structures can be adequately defined. Because full-size tests are costly and complex, scale model testing should be used. To have "proper simulation," the tests should provide good scaled simulation of both the vehicle and the plume, otherwise techniques for applying the test results to a full-scale condition must be developed. There are, however, two primary problems involved in this simulation. One involves scaling a model in the flow field, (the same problem is encountered in conventional wind tunnel testing of aerodynamic configurations and is scaled on the basis of Reynolds number and Knudsen number), the second problem involves simulating the gas dynamics of the flow properties of the rocket exhaust plume. Both problems must be satisfactorily resolved in order to obtain correctly scaled impingement forces from scale model testing.

The exhaust plumes of a rocket that operates in a near vacuum are characterized by three flow regimes, (1) continuum center portion, (2) a transitional regime surrounding the continuum region, and (3) a highly expanded free molecular regime which may include flow expanding to a direction more than 90 degrees away from the nozzle centerline. The

experimental evaluation of the forces on bodies from such plumes requires that the local plume parameters and model parameters be scaled exactly, or that techniques be provided to relate and correct the test results to full-scale conditions. The basic problem is complicated by the fact that in many instances (due to test facility limitations) the plume itself will be modeled with a gas which is different than that of the full scale system. Gas dynamic relationships between the model and the full-scale system must therefore be established in terms of

- Plume gas dynamic properties
- Reynolds number of the model in the plume
- Knudsen number of the model in the plume
- Scale model motor chamber conditions and nozzle geometry
- Condensation considerations

With these facts in mind a survey on plume scaling was made of state-of-the-art literature. Using results of the survey as a base, a computer program was written which performs a rapid search of possible simulant gas mixtures and selects the mixture that best simulates the prototype plume based on Mach number and momentum considerations. The impingement forces predicted by the model simulation are then adjusted by a momentum correction factor to account for discrepancies in the gas dynamic simulation.

In the following technical discussion, the more important sources of information are discussed, techniques used in the computer program to test and select a gas mixture are outlined and two sample cases that have been run to provide experience with the method are presented. Results for these two cases show that a simulant gas mixture can be selected which will approximate in a scaled experiment the impingement forces on a body immersed in a prototype nozzle plume.

Section 2
TECHNICAL DISCUSSION

An integral part of the plume scaling study was a literature survey carried out to obtain a working knowledge of accomplishments in the past several years in the field of scaling techniques. Thus, before the approach taken in the current study is described, the work carried out by others is outlined. Problems or limitations of the existing methods are examined, which have pointed the way to development of the procedures used in the current effort. The work applicable to this study is centered in two areas (1) general scaling of plumes, and (2) analytical models of the plume. These subjects are discussed in the following subsections.

2.1 LITERATURE REVIEW

Templemeyer (Ref. 1) performed a most pertinent study of the simulation of hot jet exhaust with mixtures of cold gases. Since the exact parameters that need to be satisfied in order to simulate one gas with another are not readily obvious, Ref. 1 examined a gaseous flowfield and found that by equating specific heat ratio, specific internal energy, pressure ratio and mass flow per unit area, the simulation between a prototype and model was achieved at the exit plane of a nozzle. By assuming a perfect gas with constant specific heats, the equations can be reduced to a set of three linear algebraic equations with weight fractions as the unknowns. Reference 1 then solved the following set of equations:

$$C_{vp} (T_{op}/T_{om}) = n_1 C_{v1} + n_2 C_{v2} + n_3 C_{v3} \quad (1a)$$

$$R_p (T_{op}/T_{om}) = n_1 R_1 + n_2 R_2 + n_3 R_3 \quad (1b)$$

$$1 = n_1 + n_2 + n_3 \quad (1c)$$

where the simulant mixture is made up of three gases. By selecting a combination of gases Eqs (1) can be solved to provide the weight fractions, N_1 . If the weight fractions are all real numbers, the gas mixture is a possible simulant.

With the solution of the above equations, the inviscid flow of a nozzle can be simulated for certain cases. The boundary layer thickness ratio (δ/D_e) can be duplicated by duplicating the Reynolds number, or

$$\rho M \sqrt{\frac{\gamma P}{\rho}} \frac{l}{\mu} \Big|_p = \rho M \sqrt{\frac{\gamma P}{\rho}} \frac{l}{\mu} \Big|_m \quad (2)$$

Since

$$M_p = M_m, \quad \gamma_p = \gamma_m, \quad P_p = P_m$$

is assumed, then

$$l_m = l_p \left(\frac{\mu_m}{\mu_p} \right)$$

Now since the viscosity of a hot exhaust gas is generally large compared to a cold gas mixture, it is difficult to achieve Reynolds number duplication if the nozzle length is to scale. As a result, Ref. 1 resorted to computing a scale factor by which the nozzle length is varied in order to achieve viscous similitude. For example in Ref. 1 a turbulent boundary layer was assumed and then the boundary layer thickness was expressed as

$$\delta = l / R_N^{0.2}$$

and

$$\delta_p \text{ (SF)} = \delta_m$$

Then

$$\left(\frac{l}{\rho u l} \frac{l}{\mu} \right)^2 \Big|_p \text{ (SF)} = \left(\frac{l}{\rho u l} \frac{l}{\mu} \right)^2 \Big|_m$$

Reducing

$$l_m = \left[(SF) \left(\frac{\mu_p}{\mu_m} \right)^{0.2} l_p^{0.8} \right]^{1.25}$$

Thus the viscous and inviscid one-dimensional flow properties will be duplicated at the exit plane. Several combinations of hydrocarbons were then found that fulfilled the necessary requirements for simulation of the exit plane properties of a turbojet engine.

Marsh (Ref. 2) developed a technique for searching for combinations of gases that duplicate the exit plane conditions of a rocket nozzle to provide plume flowfield simulation. Real gas effects were included in the analysis by a variable ratio of specific heats. Basically the following three similarity laws involving P, M, and μ were satisfied:

Pressure Ratio $(P_a/P_e)_m = (P_a/P_e)_p$ (5a)

Nozzle Lip Turning Angle

$$\left. \frac{\gamma_e M_e^2}{\sqrt{M_e^2 - 1}} \right|_m = \left. \frac{\gamma_e M_e^2}{\sqrt{M_e^2 - 1}} \right|_p$$
 (5b)

Viscosity

$$\frac{D_p}{D_m} \sqrt{\frac{l_m}{l_p} \left(\frac{\mu_m}{\mu_p} \right) \left(\frac{\rho_m}{\rho_p} \right) \left(\frac{u_m}{u_p} \right)} = 1$$
 (5c)

These requirements reduce to the necessity of duplicating γ_e , M_e , and $(\rho U/\mu)_e$. Reference 2 computed these parameters as a function of pressure ratio, chamber temperature and gas mixture. By plotting the data it was possible to determine graphically a binary or ternary mixture of gases which approximate the prototype conditions. The gas mixture generally contained one gas with a low specific heat ratio and one with a high specific heat ratio.

Gopin (Ref 3) was also interested in duplicating flowfield conditions near the exit plane of a rocket nozzle and he included the additional requirement that the impingement forces due to the exhaust gases shall be similar. With this in mind, Ref 3 then specified that the momentum flux per unit area be similar

$$\text{That is, momentum flux} = \rho u^2 A \quad (6a)$$

Since $\rho = P / RT$

$$u^2 = a^2 M^2 = \gamma RT M^2$$

Then, momentum flux = $\gamma M^2 P A$ (6b)

Equating prototype and model conditions

$$\gamma M^2 P \Big|_p = \gamma M^2 P \Big|_m \quad (6c)$$

Reference 3 points out that by choosing high density gases, which is almost synonymous with gases having multiple species, a high mass flow rate can be attained. Assuming isentropic perfect gas relationships, Ref 3 shows that

$$\begin{aligned} m/A &= \rho u = P / RT \\ m/A &= \frac{P_0}{\left(1 + \frac{\gamma-1}{2}\right)^{\gamma/\gamma-1}} \sqrt{\frac{\gamma}{RT_0 \left(\frac{2}{\gamma+1}\right)}} \\ &= \sqrt{\left(\frac{\gamma+1}{2}\right)^{-\frac{\gamma+1}{\gamma-1}}} P_0 \sqrt{\frac{\gamma}{RT_0}} \end{aligned} \quad (7)$$

If P_0 , T_0 , and γ are assumed to be constant, then mass flow is a direct function of molecular weight. Choosing polyatomic gases (multiple atomic species) provides a high mass flow per unit area with a low flow rate of molecules. Thus, it becomes much easier to maintain a vacuum

chamber at a high simulated altitude, (i.e., low pressure) for a longer period of time. Finally, to avoid condensation the simulant gas mixture was heated.

With these stipulations in mind, Ref. 3 selected several binary gas mixtures from a group of gases that were presumed to have desirable simulation traits. An experimental program was undertaken using a mixture of argon and sulfur hexafluoride to simulate the exhaust gases of the J-2 engine. Force measurements were made for impingement of the exhaust on an S-II afterbody. The major results of interest here are

- Generally there was little change in forces due to a change in specific heat ratio from $1.18 \leq \gamma \leq 1.28$, but there was significant variation for $1.28 \leq \gamma \leq 1.40$.
- Although changes in γ result in modifications of the momentum distribution in the exhaust flow field, very small variations have little effect on impingement forces. Hence, minor errors in the gas mixture used to simulate γ are negligible.

Note that in Ref. 3, $M_{e_p} = M_{e_m}$, and thus for similarity, $\gamma_{e_p} = \gamma_{e_m}$. The authors admit that simulating the exit plane momentum by simulating the specific heat ratio is only an assumption, an assumption that has been justified by previous experimental work. (This point is discussed further in Section 2.2.1.)

References 4, 5 and 6 are also interested in simulating the impingement of a highly expanded plume on a nearby surface. In particular it was desired to simulate the impingement of exhaust gases from the APS ullage motor and the O_2H_2 burner motor on the J-2 engine of the S-II stage. The added requirement that non-continuum effects be duplicated makes Refs. 5 and 6 different from the works previously mentioned.

In designating the experimental conditions, nitrogen gas was selected as the simulant gas since it came closer than any other single gas to

matching the prototype engine gas characteristics. Also of importance was the fact that nitrogen is readily pumped by helium cryopanel (as are most gases except hydrogen). To achieve proper nozzle exit plane conditions area ratios were selected that would produce the proper Mach number at the exit plane. Simulation of Knudsen number throughout the flow field was obtained by duplicating the nozzle exit plane Knudsen number.

If flowfield similarity is assumed, as noted above, scaling parameters between model and prototype conditions can be computed.

First

$$K_n = \lambda / D \quad (8)$$

Where

$$\lambda \sim m / \sigma^2 \rho \quad (9)$$

Solving for ρ and writing a ratio

$$\rho_p / \rho_m = (SF) \frac{\sigma_m^2 \psi_p}{\sigma_p^2 \psi_m} \frac{K_{nm}}{K_{np}} \quad (10)$$

Thus the density ratio provides scaling of non-continuum gas dynamics between prototype and model. To obtain a pressure scale factor between model and prototype conditions it is assumed that pressure can be written

$$P = P_{cont} + a (P_{FM} - P_{cont}) \quad (11)$$

Where a is assumed to be of the form

$$a = e^{-\frac{1}{K_n}} \quad (12)$$

and K_n is based on R_b the local body radius. Now if Mach number and momentum flux (Eq 6b) are similar, then scaling relations can be developed to match Knudsen number. Or

$$\frac{(P_s - P_{cont})_m}{(P_s - P_{cont})_p} = \frac{e^{-1/K_n}}{e^{-1/K_n}}$$

And

$$P_{s_p} = (P_s - P_{cont}) \left(\frac{a_m}{a_p} \right) + P_{cont_p} \quad (13)$$

These scaling parameters (Eqs 10 and 13) produced remarkable agreement between prototype and model conditions of Refs. 5 and 6.

In Ref 7, a rocket plume was simulated by the actual combustion of gaseous fuels to simulate the exhaust of a liquid propellant rocket engine. A shock tube technique which permitted short run times was used to maintain proper background pressure. This technique provided for the duplication of stagnation enthalpy and a good approximation to the desired molecular species concentration. The Mach number in the nozzle can be reproduced by simple geometric similarity since the boundary layer was made to scale by maintaining the full scale Reynolds number. Full scale Reynolds number was attained by increasing the chamber density. This technique has several advantages, the most obvious in that the prototype species concentration can be obtained in the model plume. Also by the simple expedient of raising the chamber pressure, the proper Reynolds number can be attained. A drawback pointed out in Ref 7 is that the steady state flow conditions over a complex body with concave shapes cannot be obtained in the testing time available.

To obtain the proper mixture of gaseous reactants to duplicate the combustion products of liquid propellants, two basic rules given in Ref 8 are used.

- 1 The atomic composition (i.e., atomic species and atom ratios) of the liquid and gaseous propellants must be the same
- 2 The initial energies of the two propellant combinations must be equivalent (i.e., the quantities must be the same) $\sum_{j=1}^r n_j (H_{T_1})_j$

Condition 1 is easily satisfied, however, condition 2 involves a trial and error approach to arrive at a proper mixture of gaseous components

Many techniques (Refs 1 through 7 were some of the most pertinent) have been employed to simulate the flow field of a rocket engine. Some techniques appear more applicable to the problem of this present effort for which the basic objectives of the present effort are related here. First, a mixture of non-reacting gases is used to simulate plume impingement forces for the hot products of combustion of a liquid propellant engine. Second, conditions in the far flow field of a plume are to be duplicated rather than conditions near the exit plane of a nozzle. This stipulation leads to the second section of this literature review.

2.1.1 Models of plumes

To simulate the conditions in a highly expanded plume, flowfield parameters in the far field region must be predicted. After a method is developed that permits the flow field to be predicted, various combinations of gases can be used to simulate the desired flowfield parameters of the prototype plume. Many documents first published in this area were basically interested in simulating jet boundary conditions near the nozzle. Representative reports are briefly reviewed in the following paragraphs for this problem. More extensive discussions which should prove useful in the present study, are then given to models of plumes.

Assuming that there is a finite back pressure, the expression for the Prandtl-Meyer expansion angle can be written

$$\frac{\Delta P}{P} = \frac{\gamma M^2}{\sqrt{M^2 - 1}} (\Delta \nu) + \text{higher order terms} \quad (14)$$

Thus Goethert (Ref 9) proposed to match the parameters $\gamma M^2 / \sqrt{M^2 - 1}$ and θ_j in order to duplicate the jet boundary of a highly underexpanded jet. Pindzola (Ref 10) carried out a study in which better boundary similarity was obtained by matching θ_j and $\gamma M^2 / \sqrt{M^2 - 1}$, where the Mach number is now based on the boundary conditions rather than on the nozzle exit conditions. Finally, in a later study Herron (Ref 11) concluded that even better simulation was obtained by matching the parameters θ_j and M / γ . All these results were obtained through experimental research.

As shown, these studies are not quite applicable to the problem currently under study, however, they were mentioned to underline previous work in jet plume simulation. Although the present effort is directed toward simulating plumes at high altitudes, it may prove useful at some later date to add the capability of simulating the shape of a plume near the nozzle. With this in mind, attention is now turned to the problem of similarity parameters for highly expanded plumes far downstream. Little work has been done previously in the area which is the objective of the present study.

To accomplish this objective the first task is to predict flowfield conditions for a highly underexpanded rocket nozzle of given conditions. The method-of-characteristics solution has been shown to be a highly accurate technique to describe analytically the flow field of a rocket plume. The method is accurate even for highly expanded plumes (Ref. 11). Method-of-characteristics solutions are relatively fast on a computer, however, for far field flow prediction, a source flow model has been found to be faster and to agree closely with method-of-characteristic solutions (Fig 1). A description of this method as given by Ref. 12 is next outlined.

Consider the exhaust jet of an ideal inviscid gas issuing isentropically into a vacuum. The flow is steady and the ratio of specific heats is constant. At large distances from the nozzle the streamlines seem to emanate from a source near the nozzle exit. It is then assumed that the pressure rapidly approaches zero and thus the velocity can be assumed to be constant. The

density then takes the form $\rho \sim 1/h^2$, where h is the radial distance from the nozzle exit (Fig 2 from Ref 13). It is assumed that the density on a spherical cap of distance h is of the form,

$$\rho / \rho_e = \frac{E}{2} \left(\frac{h}{r_e} \right)^{-2} \cos^N \theta \quad (15)$$

Then solving the equation of continuity and momentum for the unknown constants N and E , (Ref 12) obtains the following expression for Mach number

$$M = \left[\frac{2}{\gamma-1} \left\{ \left[\frac{E(A_t)}{2(A_e)} \left(\frac{h}{r_e} \right)^{-2} (\cos\theta)^{E-1} \left(\frac{\gamma+1}{2} \right)^{\frac{1}{\gamma-1}} \left(\frac{\gamma-1}{\gamma+1} \right)^{\frac{1}{2}} \right]^{1-\gamma} - 1 \right\} \right]^{\frac{1}{2}} \quad (16)$$

Thus Mach number is dependent only upon the location in the flow field for a given gas and nozzle geometry. The most obvious shortcoming of this analysis is the restriction to systems with a constant ratio of specific heats

References 14 and 15 also discuss the similarity of highly expanded rocket exhausts. These references, however, are devoted to the description of flow fields inside a barrel-shaped shock emanating from the Prandtl-Meyer expansion fan. Thus, these studies are not quite applicable to the current problem which considers expansion into a vacuum.

This brief discussion concludes the literature review of simulation parameters and plume models. The techniques outlined in the next section draw liberally from the sources which were discussed. In many cases, slightly different methods are employed because of complicating factors in the problem at hand.

2.2 METHOD OF APPROACH

Obviously a simulation of a full-scale rocket plume could be attained by duplicating Reynolds number, chemical species, Mach number, stagnation

enthalpy, and environmental pressure. Noncontinuum effects would automatically be satisfied, since Knudsen number is defined by the Mach number and Reynolds number. Since in the present analysis the chemical species cannot be simulated, the Mach number distribution will not necessarily be identical throughout the prototype and model plumes. In addition, simulating stagnation enthalpy as obtained by Ref. 6 is difficult, since the extremely high total temperature attained in the prototype case is out of the range of the experimental test equipment that is available.

As an introduction to the problem of simulation, the rules of flowfield similarity are reviewed here. With this requirement in mind, the model established to analytically test a gas for simulation ability is discussed. The computer program which was written to select a simulant gas mixture is next described. Finally, analytical results comparing impingement forces predicted from model conditions are compared with those predicted for prototype conditions.

2.2.1 Similarity Parameters

For two flow fields to be comparable in the region of interest, the terms in the equations of flow must be similar. To simplify the calculations, the analysis is carried out one-dimensionally. Writing the one-dimensional flow equations,

Momentum

$$u \frac{du}{dx} = \frac{1}{\gamma M^2} \frac{dP}{dx} + \frac{1}{R} \frac{d^2u}{dx^2} \quad (17)$$

Energy

$$u \frac{dT}{dx} = \frac{1}{P_r R_n} \frac{d^2T}{dx^2} + (\gamma - 1) M^2 u \frac{dP}{dx} + \frac{4}{3} \frac{(\gamma - 1) M^2}{R_n} \frac{d^2u}{dx^2} \quad (18)$$

Equation of State

$$P = \rho RT \quad (19)$$

Continuity

$$\frac{d(\rho u)}{dx} = 0 \quad (20)$$

The equations of state and continuity add no new information to the dimensional analysis and are included only for the sake of completeness. Thus, from momentum, equivalent terms from the model and prototype situations can be equated. On

$$\gamma_p M_p^2 = \gamma_m M_m^2 = f_1 \gamma_p f_m^2 M_p^2$$

where f_1 is a scale factor for the 1th variable

Then

$$f_m = \frac{1}{\sqrt{f_1}} \quad (21)$$

Similarly, from the energy equation

$$(\gamma_p - 1) M_p^2 = (\gamma_m - 1) M_m^2 = (f_1 \gamma_p - 1) f_m^2 M_p^2$$

Or

$$(\gamma_p - 1) = (f_1 \gamma_p - 1) f_m^2$$

Substituting from the momentum equation into the energy equation yields

$$f_1 = 1 \quad (22)$$

Thus for complete flowfield similarity, all of the following parameters must be equated

$$\gamma_p = \gamma_m \quad (23a)$$

$$M_p = M_m \quad (23b)$$

$$Rn_p = Rn_m \quad (23c)$$

$$P_{rp} = P_{rm} \quad (23d)$$

Complete similarity may never be achieved, however, since the primary interest in this study is the force produced on a body immersed in a rocket exhaust plume. Conditions leading to force similarity are examined. The force exerted on a body can be written in the general form

$$F = G(\rho, u, l, \mu, a) \quad (24)$$

Using dimensional analysis, the expression can be written in a familiar form

$$\frac{F}{\rho u^2 l^2} = G\left(\frac{\rho u l}{\mu}, \frac{u}{a}\right)$$

If viscous effects are ignored, then

$$\frac{F}{\rho u^2 l^2} = G(M) \quad (25)$$

But this expression can be written in more familiar terms as the pressure coefficient

$$\frac{F}{\rho u^2 l^2} = \frac{\Delta P}{\rho u^2} = G(M)$$

Or

$$C_p = \frac{\Delta P}{2 \rho u^2} = G(M) \quad (26)$$

Thus, for identical gases, if the Mach number is equal, the pressure coefficient C_p is identical. However, the pressure exerted on a body is also a function of gas composition or γ . In other words, pressure is a function of momentum flux ρu^2 and Mach number, where

$$T = \text{momentum flux} = \rho u^2 = \gamma P M^2 \quad (27)$$

Now, as shown in Ref 3, the impingement pressure can be duplicated by approximating the momentum flux. This assumption is also borne out by the work of Ref 4, in which computation of the impingement pressure by Newtonian calculations is analogous to computing the momentum flux. Thus, when a duplication of impingement pressure was desired, a simulant gas mixture has been selected on the mixture's ability to duplicate momentum flux at a point in the plume. In addition, options have been included in the computer program that will compare Mach number or Reynolds number and select a simulant gas mixture that best duplicates the parameters.

2.2.2 Gas Selection

As stated in the introduction, two objectives of the study are (1) select a binary or ternary mixture of gases to simulate in a scaled model the forces produced on a body immersed in a plume, and (2) include real gas effects in the analysis and attempt to duplicate such esoteric flowfield phenomena as condensation.

An ideal technique to strive for is to develop a closed form solution for the mixture ratios of a possible simulant gas (Ref 1). However, since real gas effects are to be included in the analysis, this avenue of approach is closed. If as in Refs 2, 3 and 5 duplication of exit plane conditions will

suffice to duplicate the entire flow field of interest, once again the analysis is simplified. But, as shown in Ref. 5 the immersed body is relatively close to the exit plane of the nozzle and the specific heat ratio in that region is relatively constant at 1.4. In the present study, the specific heat ratio varies from about 1.3 at the exit plane to 1.4 in the expanded region.

To duplicate this specific heat ratio, the technique suggested in Ref. 2 was adopted. Using gases suggested by Refs. 1, 3 and 16, the gases were separated by inspection into three basic groups, those which

- 1 Exhibited high γ
- 2 Exhibited low γ , and
- 3 Those that would condense relatively soon in an expanding gas

Some of the more obvious reasons for eliminating a gas from the above groups are

- 1 Toxic or easily formed toxic compounds
- 2 Cost and availability
- 3 Condensability

However, an extremely important criterion is the ability of the gas to be pumped by helium or nitrogen cryopanel in vacuum chambers. For this reason hydrogen will generally be deemed non-acceptable unless its mixture ratio in the simulant gas is very low. The actual limits are determined by the capability of the facility available for testing. One additional comment should be included concerning the thermodynamic properties of the gases used as possible simulants. Thermodynamic properties in highly expanded plumes were desirable where temperatures much below 100°K occur. Thus thermodynamic properties good down to 10°K were generated and stored on magnetic tape using the methods of Ref. 17. A list of the gases currently on the data tape which can be used as possible simulant gas components is given in Table 1.

Table 1
 GASES CURRENTLY AVAILABLE FOR ANALYSIS
 AS POSSIBLE SIMULANTS

| Chemical Formula | Name | Molecular Weight | Ratio of Specific Heats at 1 atm Pressure |
|-------------------|--------------------------|------------------|---|
| A | Argon | 39.948 | 1.667 at 86°F |
| CClF ₃ | Carbon Chlorotrifluoride | 104.465 | 1.2 at 77°F |
| CF ₄ | Carbon Tetrafluoride | 88.01 | 1.217 at 100°F |
| CHF ₃ | Trifluormethane | 70.018 | 1.22 at 30°F |
| CO ₂ | Carbon Dioxide | 44.01 | 1.3 at 86°F |
| H ₂ | Hydrogen | 2.016 | 1.4 at 86°F |
| N ₂ | Nitrogen | 28.02 | 1.405 at 26°F |
| N ₂ O | Nitrous Oxide | 44.02 | 1.303 at 59°F |

2 2 3 General Discussion of Simulant Selection Program

Using a mixture of the gases the Chemical Equilibrium Composition computer program (CEC) Ref 18, calculates the thermodynamic properties of the mixture. Then utilizing a modified source flow model, the momentum flux and Mach number at a specified point in the plume are compared to those produced by the real gas under prototype conditions also in a modified source flow plume. In addition, the Reynold's number at the exit plane is computed to ensure that the boundary layer effect is similar. The boundary layer calculation is discussed later, however, the most important point to note is that automating the computations allows possible gas mixtures to be thoroughly searched. Thus not only can the mixture ratio be varied, but the stagnation pressure and temperature can be altered within specified limits. Unfortunately, if one particular gas mixture does not meet the desired specifications, another set of gases must be tried at random. However, this is the same procedure employed in Ref 1, and no real alternative appears to be available. After a set of gases is chosen for a specified chamber temperature and pressure, it is possible to determine rather quickly if any possible combination will meet the desired criteria. This calculation is described in detail in Appendix A.

Thus, after a possible gas mixture has been selected, the ability of this gas to simulate forces on a body immersed in a plume formed from these gases must be predicted. This can be done by use, again, of a source flow model of the plume.

• Plume Source Flow Model

As illustrated in Fig 1 taken from Ref 12, the flow field computed by a source flow model predicts quite well the parameters of the far flowfield region. Since real gas effects are to be included in the analysis, the technique of Ref 12 discussed in Section 2 1 could not be used to obtain a closed

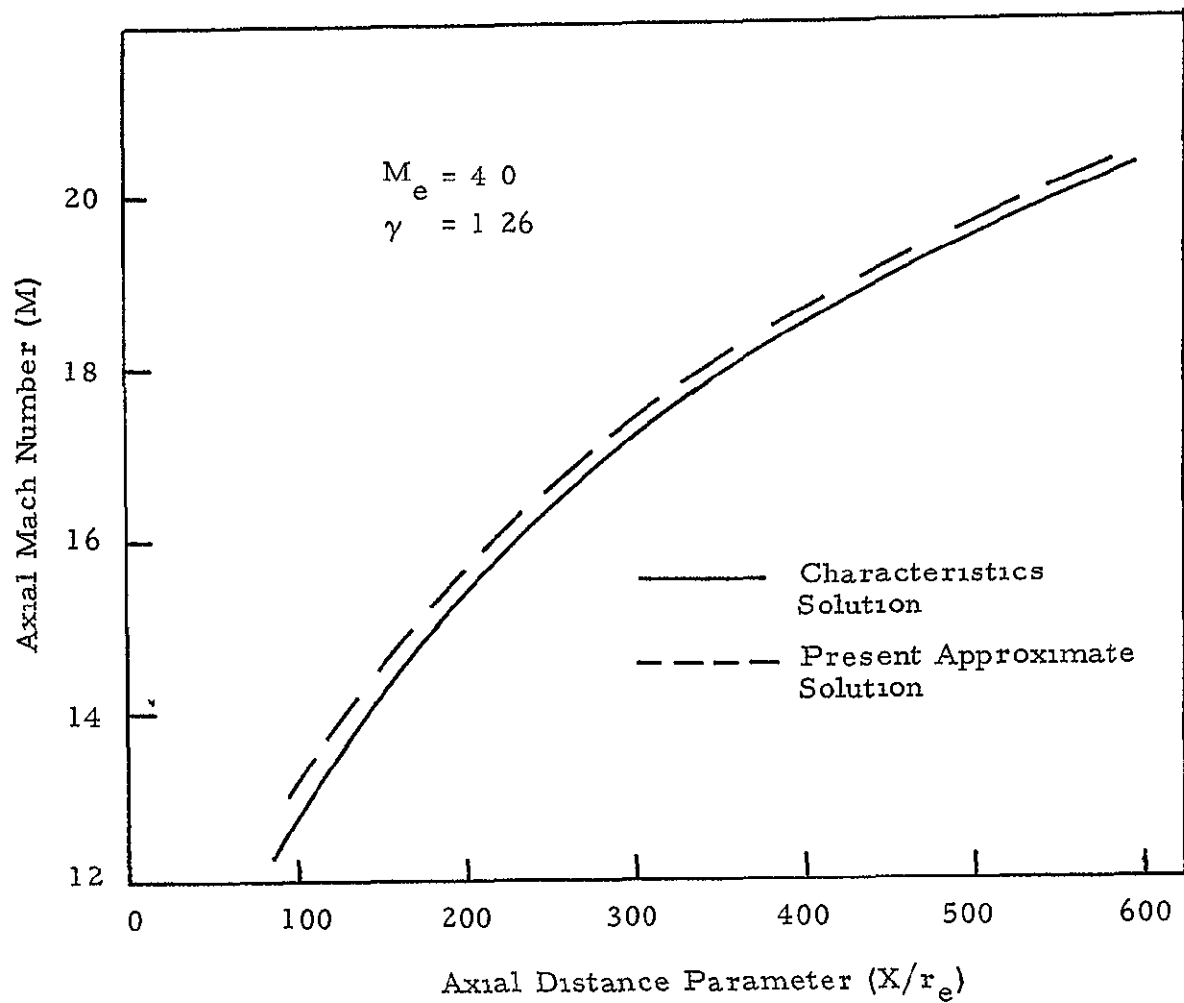


Fig 1 - A Comparison of the Approximate and Characteristics Solution for a Rocket Exhausting into a Vacuum ($M_e = 4.0$, $\gamma = 1.24$) Ref 12

form solution for the flow properties at a point. Instead, a numerical solution using the method of false position was employed to solve for the flow field properties that satisfied the specified area ratio of the flow field. In addition, rather than assuming a hemispherical flow field as Ref 12, the Prandtl-Meyer expansion angle at the nozzle lip is computed and the area ratio of the plume is calculated using this as the boundary of the plume (Fig 2). Reference 13 discusses this program more fully. The centerline Mach numbers for the RIE exhaust plume as computed by the MOC and source flow programs are shown in Fig 3 taken from Ref 13. Once again the comparison is acceptable.

After the plume is generated, corresponding points of the model and prototype plume flow fields can be compared. The technique thus produces a flexible but bulky method of determining a good simulant mixture. It should be noted, however, that not only must points in the inviscid plume be compared, but also viscous effects in the nozzle which are similar must be ensured.

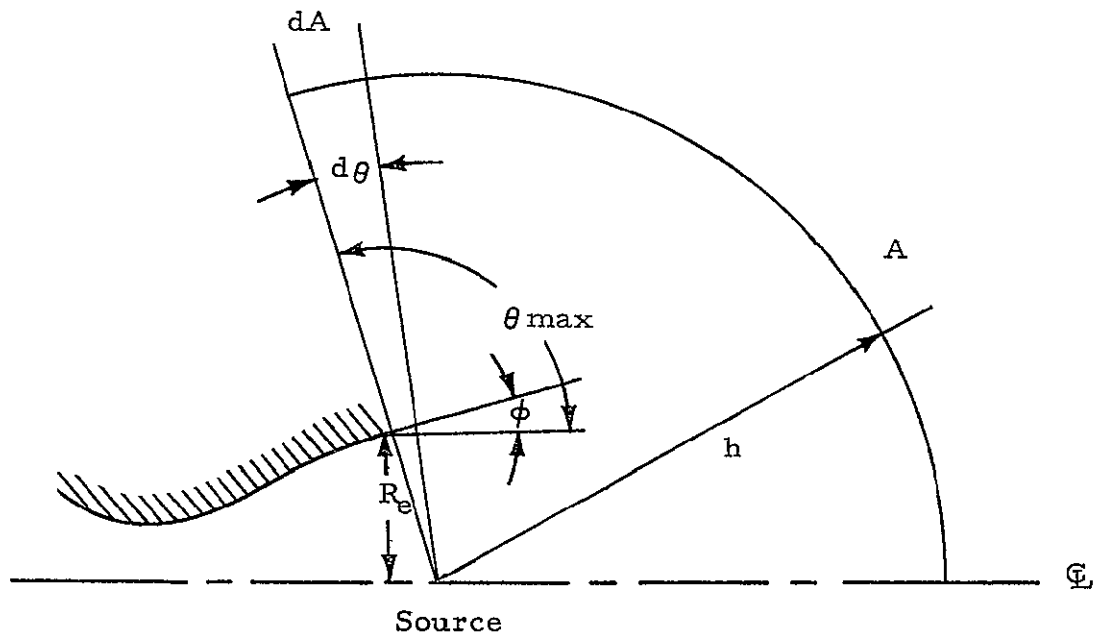
- Boundary Layer

To simulate the viscous flow effects in the nozzle the ratio, δ/D , must be equal for both model and prototype. The following analysis is carried out assuming turbulent flow in the nozzle. Similar statements can be made regarding laminar flow. In general the boundary layer thickness can be written as a familiar function of Reynolds number

$$\delta/l = k \left(\frac{\rho u l}{\mu} \right)^{-1/5} = k \left(R_l \right)^{-1/5} \quad (28)$$

where k is a constant for turbulent flow and R_l is Reynolds number based on a characteristic length of the nozzle. Now obtaining a ratio of (δ/D)

$$\left(\frac{\delta}{D} \right) \frac{1}{l} = \frac{k}{d^{4/5} l^{1/5}} \left(\frac{1}{R_D} \right)^{1/5}$$



θ_{\max} = Prandtl -Meyer Expansion Angle

ϕ = Nozzle Lip Angle

Fig 2 - Source Flow Model of Plume Showing the Model Geometry

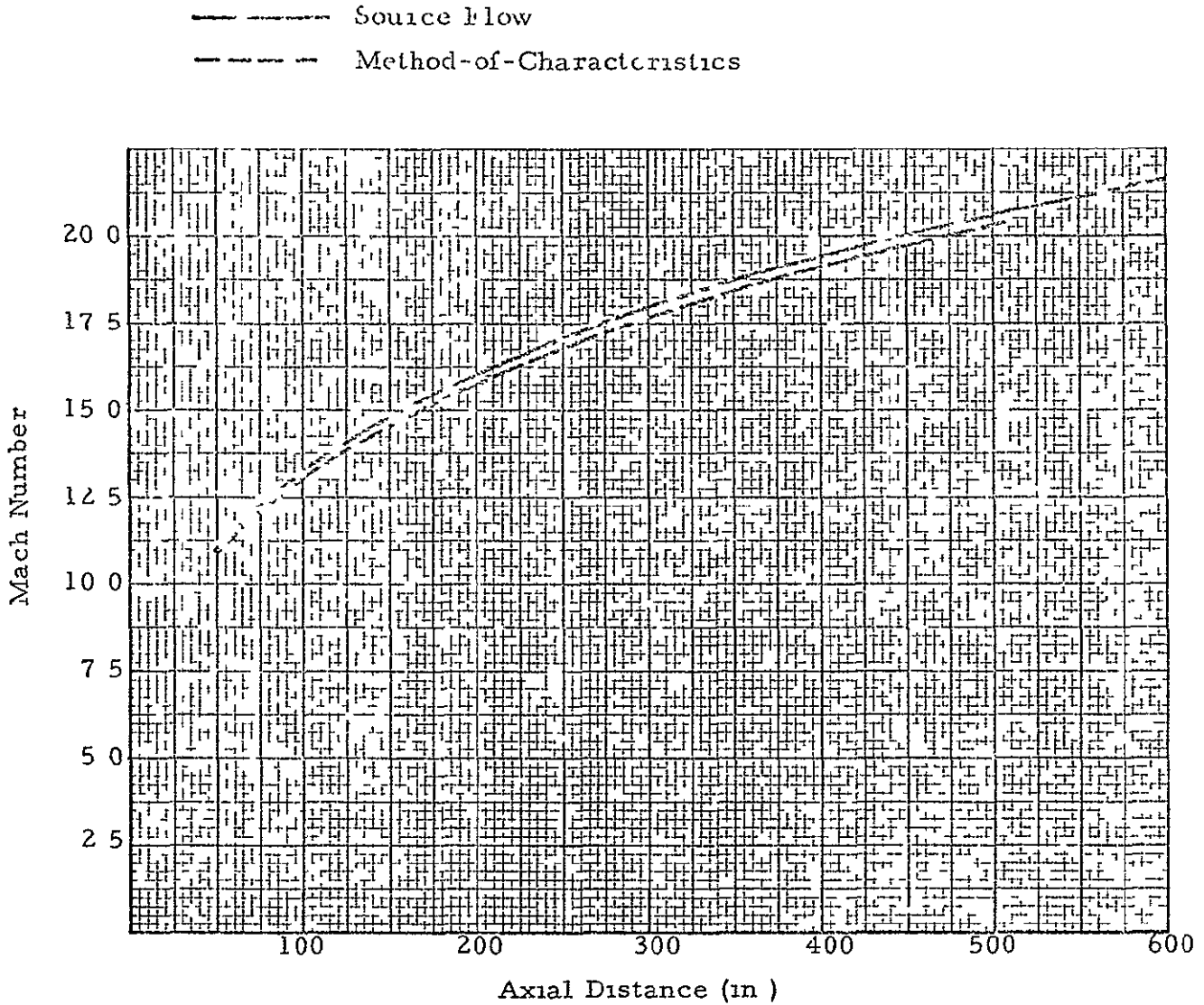


Fig 3 - Comparison of the R-1E Engine Centerline Distribution of Mach Numbers Using Data from the Method-of-Characteristics and Source Flow Computer Programs ($\gamma = 1.259$)

or

$$\left(\frac{\delta}{D}\right) = k \left(\frac{l}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \quad (29)$$

Equating the ratio for model and plume cases

$$k \left(\frac{l}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_m = k \left(\frac{l}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_p$$

Thus

$$\left(\frac{l}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_m = \left(\frac{l}{D}\right)^{4/5} \left(\frac{1}{R_D}\right)^{1/5} \Big|_p \quad (30)$$

Now if Reynolds number can be duplicated, then near geometric similarity assures similitude. However, from Refs. 1 and 2 it may be difficult to duplicate Reynolds number. In order to ensure viscous similarity it may be necessary to modify the length of the model nozzle, or

$$\begin{aligned} l_m^{4/5} &= \left(\frac{D_m}{D_p}\right)^{4/5} l_p \left(\frac{R_{Dp}}{R_{Dm}}\right)^{1/5} \\ &= (SF)^{4/5} l_p^{4/5} \left(\frac{R_{Dp}}{R_{Dm}}\right)^{1/5} \\ l_m &= (SF) l_p \left(\frac{R_{Dp}}{R_{Dm}}\right)^{1/4} \end{aligned} \quad (31)$$

In the present study the primary concern is that the boundary layer shall be no greater in the model situation than in the prototype situation. To meet this requirement, the simulant selection program specifies that the Reynolds number of the model must be equal to or greater than the Reynolds number of the prototype nozzle. Transport properties of the gases in question are computed, using the methods reported in Ref. 19.

For the sake of completeness, a modified nozzle length can be calculated after a gas mixture has been established for a specified chamber condition. Besides simulating the basic flowfield parameters (such as Mach number and Reynolds number) one other phenomenon, condensation, must be matched.

- Condensation

Generally, in highly expanded rocket plumes having temperatures well below 100°K, heterogeneous systems are of considerable importance. In particular, as the partial pressure of each gaseous component drops below its vapor pressure, the probability of the formation of liquid droplets increases. In general, the theory of condensation is felt to be understood. In fact, calculations of condensation in steam nozzles or of water vapor in air seem to bear out this theory. See for example Refs. 20 and 21. Unfortunately, corresponding calculations cannot be as easily made for the gaseous substances such as nitrogen or carbon dioxide. Much of the problem lies in the lack of accurate knowledge of material properties such as surface tension and density. The problem may be illustrated by writing the expression for fractional formation rates (Ref. 20)

$$\frac{1}{N_g} \frac{dN_g}{dT} = g^* \frac{J(g^*)}{N_g} = \frac{P}{kT} \frac{4r_d^3}{3} \sqrt{\frac{2\pi\zeta}{m}} e^{-4\pi\zeta r_d^2 / 3kT} \quad (32)$$

The dominant term in the expression is the exponential

$$e^{-4\pi\zeta r_d^2 / 3kT} \quad (33)$$

which may be written

$$e^{-16\pi\zeta^3 V_{liq}^2 / 3(kT)^3 \ln(P/P_{s\infty})} \quad (34)$$

Since surface tension ζ is a cubed quantity, any error in it greatly alters the computed condensation rate

Because of this problem, no attempt was made to match condensation rate. Rather, an attempt was made to duplicate only the location of condensation. Currently condensation is assumed to occur when the partial pressure of the gaseous species drops below the vapor pressure for that corresponding temperature. The point at which condensation occurs is modified by adjusting the chamber temperature. Since this adjustment could upset simulation of impingement forces or viscous effects, it is carried out last. Noncompliance with the condensation requirement does not eliminate the gas mixture, however, the search is continued for other combinations that might better duplicate the prototype flow field.

This concludes a brief description of the approach taken to simulate a plume flow field. Obviously some differences exist between the model and prototype condition. In order to analytically scale from the model to the prototype condition the following approach is used.

2.2.4 Scale Factors

After a gas mixture and chamber condition have been selected, the veracity of the choice must be tested. In order to transfer analytically from the model to the prototype case, a scale factor is defined. Although the methods of Ref. 4 were considered for use, a much simpler analytical correlation between the prototype and model cases is supplied by comparing the momentum flux in the corresponding plume regions. This factor thus corrects for mismatches of any pertinent parameters. The correction factor for momentum is designated as β where

$$\beta = \frac{(\text{momentum flux})_p}{(\text{momentum flux})_m} \quad (35)$$

This concludes the description of the method of analysis. A discussion now follows of the results obtained thus far with the simulant selection computer program

2.3 DISCUSSION OF ANALYTICAL RESULTS

Table 2 compares the operating characteristics for a prototype rocket motor and its corresponding model nozzle. For this case, the simulant gas mixture was a gaseous binary mixture. Since the simulant mixture was binary, condensation was not accounted for. Significantly, with the higher operating pressure of the model case, the exit plane Reynolds number was higher than the prototype case. Thus the boundary layer should be at least no greater a factor in the model case than in the prototype case. The ability to minimize the importance of the boundary layer for both the binary and ternary simulant mixtures greatly facilitates a search for a suitable simulant mixture. The centerline Mach number distribution is compared for the prototype and model case in Fig. 3. The error in the momentum flux at the center of the region of interest is 2%. Thus impingement forces in this region should be very closely scaled.

Again Table 2 compares the operating parameters for another prototype nozzle and its correspondent model nozzle. Now, the simulant gas was a gaseous ternary system. The additional gas CO_2 was assumed to be a condensable gas in the model system. Once again it was possible to minimize the boundary layer effect in the model case.

A rather surprising result occurred when the point of condensation or point of vapor saturation in the model and prototype plume was computed. For both cases, the point of condensation was found to occur far out in the plume. Realistically, this result may be more a reflection of the calculational methods used than of the physical situation. However, since the prototype and model calculations are independent, it appears significant that this result was obtained for both cases. Figure 3 compares the centerline Mach

Table 2

COMPARISON OF MODEL AND PROTOTYPE ENGINE
OPERATIONAL CHARACTERISTICS

| Engine | Binary Mixture | | | Ternary Mixture | | |
|-----------|---------------------------------------|---------|-------------------------|---|---------|-------------------------|
| | Gases | Percent | Chamber Pressure (psia) | Gases | Percent | Chamber Pressure (psia) |
| Model | CF ₄ | 0.6405 | 200 | CF ₄ | 0.7151 | 200 |
| | N ₂ | 0.3595 | | N ₂ | 0.0849 | |
| | | | | CO ₂ | 0.2000 | |
| Prototype | Fuel C ₂ H ₄ | 0.5 | 100 | Fuel CH ₃ NHNH ₂ | 0.5 | 100 |
| | Oxidant O ₂ | 0.5 | | Oxidant N ₂ O ₄ | 0.5 | |

number distribution for the model and prototype case. The error in the momentum flux at the center of the region of interest is 3%. Because of time limitations the two sample cases were the only results obtained to date. However, some general comments may be made concerning the simulant selection program.

First, the program is quite fast. The two cases discussed above were executing in approximately 5 to 6 minutes on the IBM 7094. From work performed while the program was being checked out, it appears that if new gases must be selected, then the run time will approximately double. Thus, it does appear that this computer program is a practical and economical tool to use in the design of an experiment to test impingement forces on bodies immersed in a plume.

A result of perhaps a more serious nature occurred for the ternary case. Here with a mixture of CF_4 , N_2 and CO_2 at elevated temperatures, some decomposition and reaction of the gases was predicted by the CEC routines. One of the resultant gases was COF_3 . This gas is quite toxic, being related to phosgene, the nerve gas. Although mixtures of CF_4 and CO_2 were used in Ref. 3, this mixture should not be used in a practical experimental situation until a thorough study of reaction rates is made. Suitable substitutes for CF_4 might be the inert gases such as neon, krypton and xenon. Krypton and xenon are rather expensive, but they are becoming more commonplace. Only neon exists on the products tape to date, however, if necessary, the others could be readily included.

Section 3

CONCLUSIONS AND RECOMMENDATIONS

In general, simulation of rocket exhaust plumes and the subsequent impingement force can be attained by using nonreacting gas mixtures in model nozzles. A computer program which performs the arduous task of selecting a suitable simulant gas mixture has been written and checked out. Although several options are available, the most important consists of selecting a simulant gas based upon its ability to duplicate momentum flux or impingement force on a body immersed in a plume. A set of gases was established which, when mixed, provide good simulation properties. Data for these gases are stored on magnetic tape. Additional gases can be added to the tape when deemed desirable. For the two test cases examined, simulant gases were obtained that duplicated the prototype case very well.

Since in an experimental situation it may be difficult with available equipment to attain the necessary parameters for exact simulation, an experimental program to examine the effects of nonsimilarity is recommended. Such a program was outlined in Ref. 22. In brief, by operating a single nozzle at several chamber conditions, the variation in impingement force with chamber enthalpy may be ascertained. Then, using two scaled nozzles -- one as model and the other as prototype -- the simulant selection program will be used to select a gas mixture for the model. Using this gas mixture in the model, impingement forces on a submerged body will be measured and compared to those for the prototype case. Facilities exist to carry out such a study and such an investigation would add validity to the analytical results developed in the current contract.

Before concluding this report this speculative note will be advanced. In order to duplicate the flow field of a gas the properties of the model gas

must be known. There is at this time some preliminary effort to use numerical techniques on electronic computers to solve the equations of quantum mechanics for various molecules (Ref 23). With techniques of this type available, a tremendous number of possible molecules could be studied and their resultant thermodynamic properties predicted. Thermodynamic properties of these molecules could then be compared with the properties of the molecules of the prototype nozzle, and a simulant gas could be selected on the basis of this comparison. Although such a study was beyond the state-of-the-art for the current effort, these techniques might be considered in future efforts.

REFERENCES

- 1 Templemeyer, K E , "An Analytical Study of Hot Jet Simulation With a Cold Gas Mixture", AEDC TN-58-54, Arnold Engineering Development Center, Arnold Air Force Station, Tenn , September 1958
- 2 Marsh, Walter R , "Gas Mixtures for Dynamic Simulation of Rocket Exhaust Jets", RMD 5804-F, Thiokol Chemical Corp , Reaction Motors Division, Denville, N J , November 1965
- 3 Gopin, A J , and E L Margolin, "A Cold Gas, Short Duration Technique for High Altitude, Underexpanded Jet Exhaust Impingement Studies," SID 64-1639, North American Aviation, Inc , Downey, Calif., September 1964
- 4 Ratliff, A , et al, "Analysis of Heating Rates and Forces on Bodies Subject to Rocket Exhaust Plume Impingements," LMSC/HREC A791230, Lockheed Missiles and Space Company, Huntsville, Ala , March 1968
- 5 Melton, H R , L M Shar, et al , "Simulation of Non-Continuum Free Jet Plume Impingements," Douglas Paper 4869, Douglas Missile and Space Systems Division (Presented to AIAA 2nd Flight Test/Simulation and Support Conference, Los Angeles, Calif , March 25-27, 1968)
- 6 Shaw, L M , and R S Hickman, "Simulation of Low Density Plumes in a Space Simulator," Douglas Paper 4444, Douglas Missile and Space Systems Division, (Presented at ASTM/IES/AIAA Second Space Simulation Conference, Philadelphia, Pa , September 11-13, 1967, Available from author).
- 7 Leng, N , R Oman, and H B Hopkins, "A Detonation Tube Technique for Simulating Rocket Plumes and Rockets," AIAA J Spacecraft Rockets, October 1968, Vol 5, No 10, pp. 1148-1154.
- 8 Sheeran, W , "Simulation of Earth Storable Liquid Propellants with Gaseous Reactants," HFD-PS-67-r, Cornell Aeronautical Laboratory, Inc , Buffalo, N Y , June 1967
- 9 Goethert, B H , and L T Barnes, "Some Studies of the Flow Pattern at the Base of Missiles with Rocket Exhaust Jets," AEDC-TR-58-12, Arnold Engineering Development Center, Arnold Air Force Station, Tenn , October 1958

- 10 Pindzola, M , "Boundary Simulation Parameters for Underexpanded Jets in a Quiescent Atmosphere," AEDC-TR-65-6, Arnold Engineering Development Center, Arnold Air Force Station, Tenn , January 1965
- 11 Herron, R D , "Investigation of Jet Boundary Simulation Parameters for Underexpanded Jets in a Quiescent Atmosphere," AEDC-TR-68-108, Arnold Engineering Development Center, Arnold Air Force Station, Tenn , September 1968
- 12 Karydas, A I , and H T Kato, "An Approximate Method for Calculating the Flow Field of a Rocket Exhausting into a Vacuum," Engineering Analysis Technical Note No 24, Philco, Aeronautics Division, Blue Bell, Pa , June 1964
- 13 Stephens, J T , "Development of a Source Flow Program to Predict the Flow Field of a High Altitude Plume," LMSC/HREC D162230, Lockheed Missiles and Space Company, Huntsville, Ala , March 1970
- 14 Sherman, F S , "Self Similar Development of Inviscid Hypersonic Free-Jet Flows," Technical Report 6-90-63-61, Lockheed Missiles and Space Company, Sunnyvale Calif , May 1963
- 15 Moran, James P , "Similarity in High Altitude Jets," AIAA J , Vol 5, No 7, July 1967, pp 1343-1345
- 16 Chapman, Dear R , "Some Possibilities of Using Gas Mixture Other than Air in Aerodynamic Research," NACA Technical Note 3226
- 17 McBride, B J , and S Gordon, "FORTRAN IV Program for Calculation of Thermodynamic Data," NASA TN-D-4097, NASA-Lewis Research Center, Cleveland, Ohio, August 1967
- 18 McBride, B J , and S Gordon, "Preliminary Description of CEC, a Computer Program for the Calculation of Chemical Equilibrium Compositions with Applications," Preliminary Report, NASA-Lewis Research Center, Cleveland, Ohio, May 31, 1967
- 19 Svehla, Roger A , "Estimated Viscosities and Thermal Conductivities of Gases of High Temperatures," NASA TR R-132, 1962
- 20 Emmons, Howard W , Fundamentals of Gas Dynamics, Princeton University Press, 1958
- 21 Wegener, P P , "Nonequilibrium Flows, Part I," Marcel Dekker, 1969
- 22 Stephens, J T , "An Experimental Investigation of Scaling Rocket Motor Plumes and the Impingement Forces on Bodies Immersed in the Plume,"

LMSC/HREC D162335, TM 54/20-253, Lockheed Missiles and Space Company, Huntsville, Ala , July 1970

- 23 Wahl, A , "Chemistry by Computer," Scientific American, April 1970, Vol 222

APPENDIX A

EFFECT OF MIXTURE RATIO ON MACH NUMBER

Appendix A

The goal of this analysis is to determine if, for specified chamber conditions, any combination of a set of gases can duplicate the conditions at a point in the prototype plume. If duplication is possible, the mixture ratio which will produce the desired conditions must be computed.

Although this search could be made simply by modifying the mixture ratio and observing the resultant change, the ability to make an intelligent estimate concerning the amount of change required is desirable. The estimate need not be exact, it merely points the iteration process in the correct direction and supplies a rough figure for the amount of change necessary in the gas mixture, given the chamber conditions. Now the simulant gas will be selected by its ability to match Mach number and momentum. Appendix B shows that for large values of Mach number, the rate of change of pressure is small compared to the rate of change of Mach number. Hence, the change in momentum becomes a strong function of Mach number.

To determine the mixture ratio, the equations of motion are employed with the definition of Mach number, all written in differential form. In this manner, when the initial mixture ratio is known, the necessary change in mixture ratio can be computed. Before proceeding with the analysis note that mixture ratio can be related to mean molecular weight of a mixture. Thus, molecular weight of the mixture is used as a variable in the following analysis. In the computer program, this is related back to mixture ratio. With this in mind the variation of flow parameters is formulated for one-dimensional flow.

The following assumptions are made

- a Flow is one-dimensional and steady
- b Changes in stream properties are continuous
- c Gas is semi-perfect, specific heat varies with composition and temperature

Writing the basic equations in differential form,

Equation of State

$$\frac{dP}{P} = \frac{d\rho}{\rho} + \frac{dT}{T} - \frac{d\psi}{\psi} \quad A 1$$

Continuity

$$\frac{d\dot{m}}{\dot{m}} = \frac{d\rho}{\rho} + \frac{du}{u} + \frac{dA}{A} \quad A 2$$

Energy

$$\frac{1}{C_p T} \frac{d\dot{m}}{\dot{m}} + \frac{1}{h_o} \left(\frac{dh}{C_p T} + \frac{\gamma-1}{2} M^2 \frac{du^2}{u^2} \right) = 0 \quad A 3$$

Momentum

$$\frac{dP}{P} + \gamma M^2 \left(\frac{dA}{A} + \frac{du^2}{u^2} + \frac{d\rho}{\rho} \right) = 0 \quad A 4$$

and the definition of Mach number

$$\frac{dM^2}{M^2} = \frac{du^2}{u^2} + \frac{d\psi}{\psi} - \frac{d\gamma}{\gamma} - \frac{dT}{T} \quad A 5$$

Now Eq (A 5) is rewritten

$$\frac{d\psi}{\psi} = \frac{dM^2}{M^2} - \frac{du^2}{u^2} + \frac{d\gamma}{\gamma} + \frac{dT}{T} \quad A 6$$

And Eqs (A 1) through (A 4) are then used to write du^2/u^2 , $d\gamma/\gamma$, and dT/T in terms of M and ψ

The equation obtained after all the algebraic manipulation is

$$\begin{aligned} \frac{d\psi}{\psi} = & \frac{dM^2}{M^2} - 2 \left\{ -\frac{h}{h_0} \left[\frac{dh}{h} - \frac{\gamma-1}{2} M^2 \left(\frac{dT}{T} - \frac{d\psi}{\psi} \right) - \frac{dA}{A} \right] \right. \\ & \left. + \frac{dh}{h} - \frac{d\psi}{\psi} - \frac{dA}{A} \right\} + \frac{d\gamma}{\gamma} + \frac{dh}{h} \quad A 7 \end{aligned}$$

Where h has been substituted for $C_p T$ to simplify the equation slightly

Now assume that h and γ are linear functions of ψ or molecular weight. Although this is not true, the assumption can be shown to yield results which are in error a maximum of 5 to 10%. See Figs A-1 and A-2 and refer to Ref 2. Changes in γ and h may then be expressed as

$$dh = m_1 d\psi \quad A-8a$$

$$d\gamma = m_2 d\psi \quad A-8b$$

The expression for the change in molecular weight or mixture ratio required to produce a desired change in Mach number becomes

$$d\psi = \frac{dM^2}{M^2} \left/ \left[\frac{1}{\psi} + \frac{2h}{h_o} \left\{ -\frac{m_1}{h} + \frac{\gamma-1}{2} M^2 \left(\frac{m_1}{h} - \frac{1}{\psi} \right) + \frac{dA}{A} \right\} + \frac{2m_1}{h} - \frac{2}{\psi} - \frac{2dA}{A} - \frac{m_2}{\gamma} - \frac{m_1}{h} \right] \right. \quad A 9$$

Now an expression for dA/A can be obtained easily by assuming an inviscid expansion at the nozzle lip and computing the change in the Prandtl-Meyer expansion angle caused by changing the gas composition. Since the nozzles under consideration in this study have large area ratios (A/A^*), assume that the gas in expansion is frozen thermodynamically. The limiting expansion angle can then be expressed,

$$\nu = \frac{\pi}{2} \left[\sqrt{\frac{\gamma+1}{\gamma-1}} - 1 \right] \quad A 10$$

Or θ , the flow, angle can be written

$$\theta = \nu - \nu_e + \phi \quad A 11$$

then the one-dimensional area of the plume at some radial distance S from the source is,

$$A = S \theta \quad A 12$$

Now with a small change in gas composition or γ the resultant area change is approximated by

$$dA = S d\theta = S \left[d\nu - d\nu_e \right] \quad A 13$$

$$v_e = \sqrt{\frac{\gamma+1}{\gamma-1}} \tan^{-1} \sqrt{\frac{\gamma-1}{\gamma+1} (M_e^2 - 1)} - \tan^{-1} \sqrt{M_e^2 - 1} \quad \text{A 14}$$

$$dv = -\frac{1}{(\gamma-1)^2} \frac{\pi}{2} \sqrt{\frac{\gamma-1}{\gamma+1}} dy \quad \text{A 15}$$

$$dv_e = -\frac{1}{(\gamma-1)^2} \sqrt{\frac{\gamma-1}{\gamma+1}} \tan^{-1} \sqrt{\frac{\gamma-1}{\gamma+1} (M_e^2 - 1)} +$$

$$2 \sqrt{\frac{\gamma+1}{\gamma-1}} (M_e^2 - 1) \left[1 + \frac{\gamma-1}{\gamma+1} (M_e^2 - 1) \right] \left[\frac{1}{2} \frac{\gamma-1}{\gamma+1} (M_e^2 - 1) \right]^{1/2} dy \quad \text{A 16}$$

$$\frac{dA}{A} = \frac{(dv - dv_e) dy}{\theta} \quad \text{A 17}$$

This expression for dA/A can then be substituted into Eq A 9 to complete the analysis. Obviously, the final expression is not strictly correct, however, it does allow an estimate of the change required in gas mixture to obtain the desired parameter.

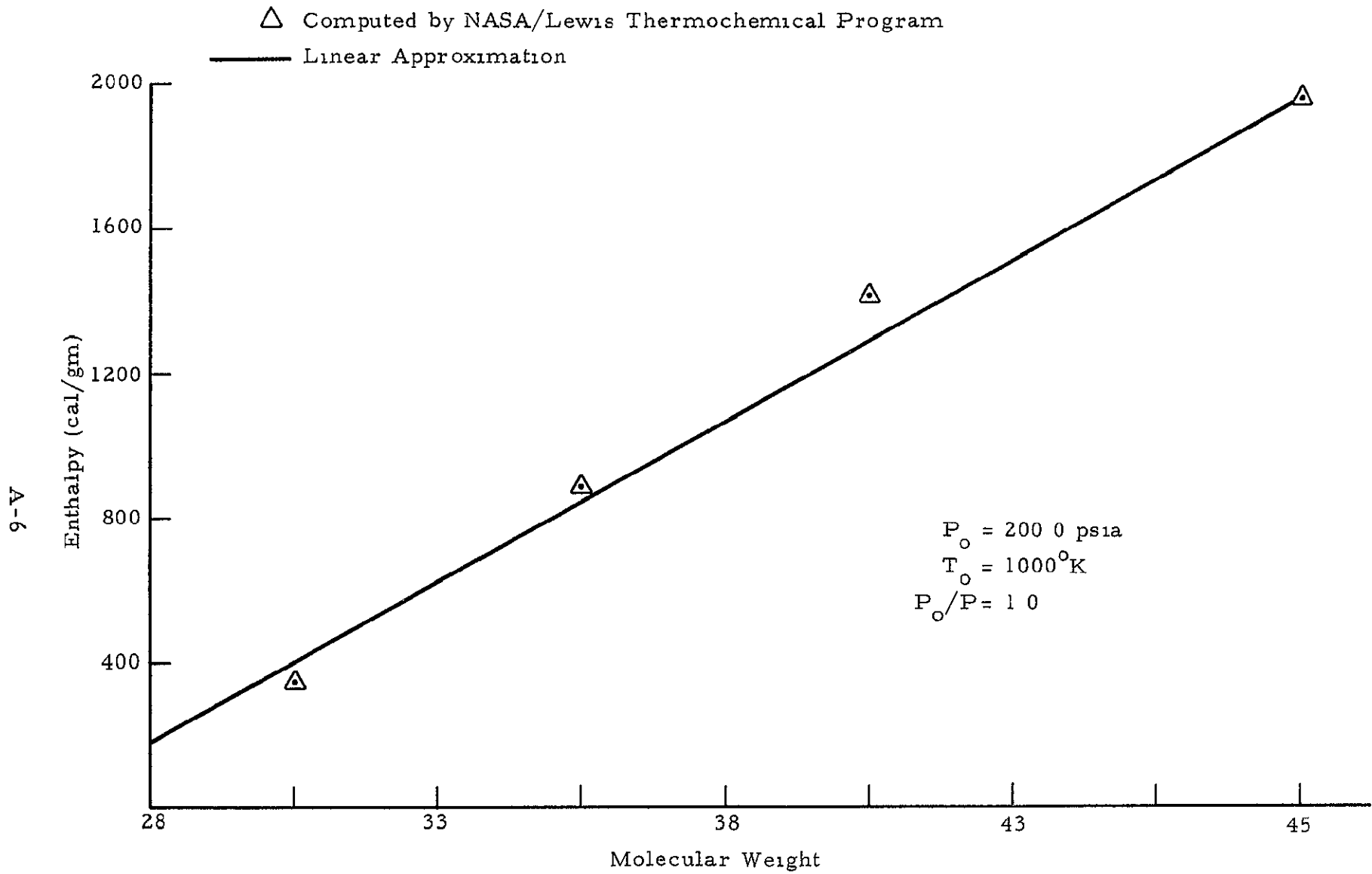


Fig A-1 - Enthalpy Versus Molecular Weight for Various Mixtures of Gaseous Nitrogen and Carbon Dioxide

A-7

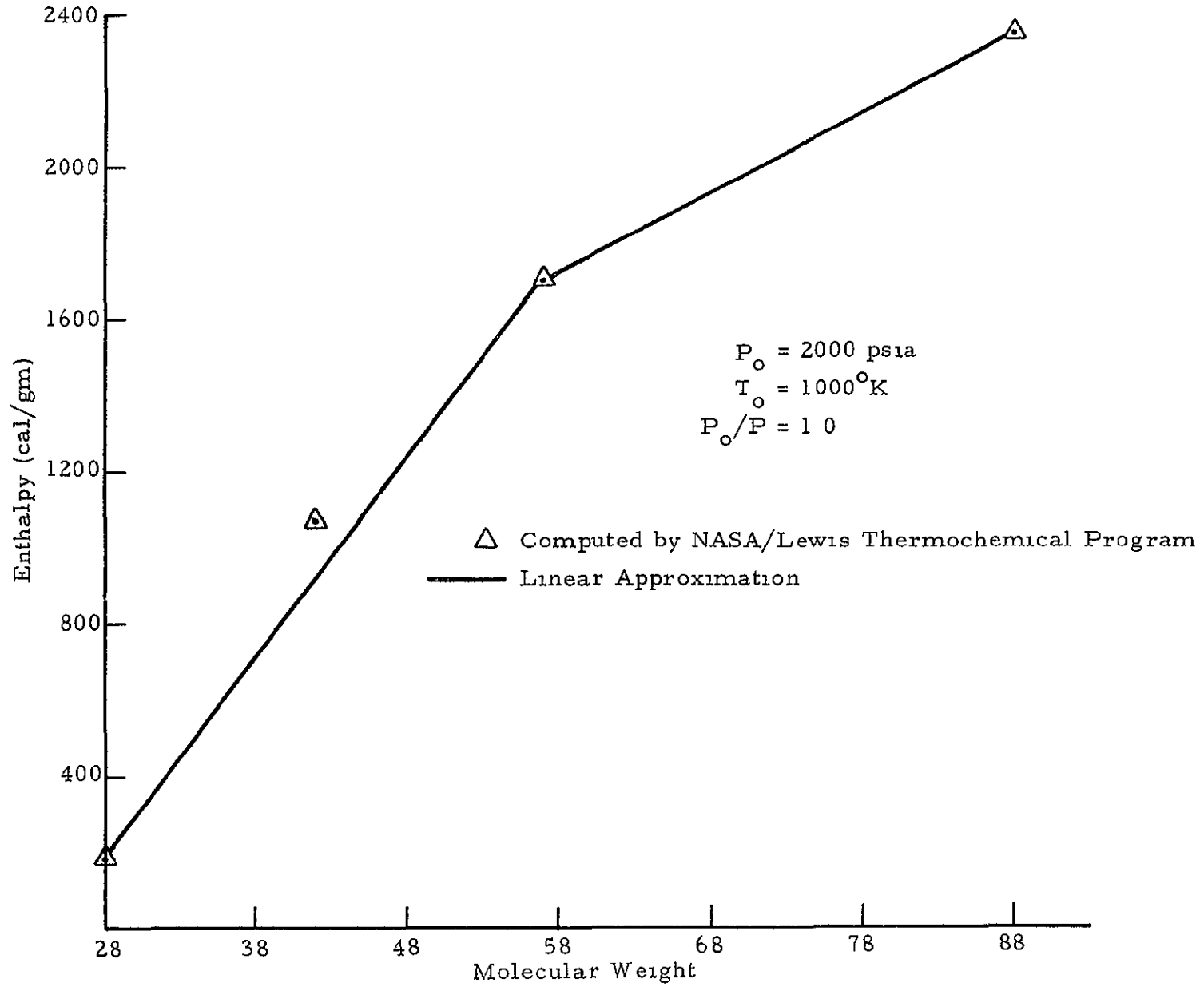


Fig A-2 - Enthalpy Versus Molecular Weight for Various Mixtures of Gaseous Nitrogen and Carbon Tetrafluoride (CF_4)

APPENDIX B

ISENTROPIC EXPANSION IN TERMS OF THE
VARIABLES PRESSURE AND MACH NUMBER

"

Appendix B

Assuming isentropic conditions hold at a point, then we may write

$$P = P_o / \left(1 + \frac{\gamma-1}{2} M^2 \right)^{\gamma/\gamma-1} \quad (B-1)$$

Now let M change by an amount ΔM Then

$$\Delta P = \frac{P_o}{\left[1 + \frac{\gamma-1}{2} (M^2 + 2M\Delta M + (\Delta M)^2) \right]^{\gamma/\gamma-1}} - \frac{P_o}{\left(1 + \frac{\gamma-1}{2} M^2 \right)^{\gamma/\gamma-1}} \quad (B-2)$$

assuming some typical values for P_o , M and γ in an expanded plume,

$$P_o = 1000$$

$$\gamma = 1.4$$

$$M = 20$$

Then for a 10% change in M,

$$\Delta P = 0.059 \times 10^{-3}$$

Since ΔP is an inverse function of M, it obviously becomes greater for smaller Mach numbers. However, the region of interest in this project is the highly expanded region and in that case changes in pressure are small for changes in Mach number.

APPENDIX C

USER'S MANUAL

DESCRIPTION OF A DIGITAL COMPUTER PROGRAM FOR
SELECTING A GAS MIXTURE TO SIMULATE THE PLUME OF A
ROCKET NOZZLE

Appendix C

C.1 INTRODUCTION

To determine accurately impingement forces on complex bodies immersed in the plume of a rocket nozzle experimental testing on scale models of the prototype situation is needed. To simplify the experimental procedure nonreacting cold gases should be used to simulate the plume. If cold nonreacting gases are introduced in the test situation, duplication of the entire prototype plume is impossible and selecting a simulant gas mixture becomes difficult.

To overcome the numerical magnitude of selecting the simulant, Lockheed Missiles & Space Company, Huntsville Research & Engineering Center, developed under contract to the Aero-Astrodynamics Laboratory of Marshall Space Flight Center, a digital program which rapidly searches among possible simulant gases to determine a gas mixture that best approximates a region in the prototype plume. The program is applicable for problems involving the high altitude expansion of a nozzle exhaust. Input to this program has been kept as simple as possible in order to enhance the usefulness of the program.

This document was prepared to facilitate operation and understanding of the program. Questions involving initial assumptions made in this program can be answered by referring to the main body of this report. Inevitably questions will arise concerning any newly created program. These should be referred to the author.

C 2 DISCUSSION

The program consists of 28 active subroutines or functions which perform the gas thermodynamic calculations, the source flow expansion and the comparison of prototype and model plumes. A general flow chart of the method of solution is given in Figure C-1. In addition, the overlay structure necessary for use on the IBM 7094 computer is illustrated in Fig C-2.

The Input procedure and output interpretation is covered in the Input/Output Section. The input instructions are simple and self-explanatory. The output instructions are in the form of flagged comments which refer to a corresponding section on a typical page of output. An IBM 7094 Instruction card is included at the end of the Input/Output Section.

To aid in the study of this program a commented listing of the program is included in this document as Appendix D.

Table 1 of the basic report tabulates the gases which are currently stored on the master tape as possible simulant gases. This array can be expanded using results from Refs 17 or 18.

Table C-1 (From Table 1)

| Gases Currently Available for Analysis as Possible Simulants | |
|--|--------------------------|
| Ar | Argon |
| CClF ₃ | Carbon Chlorotrifluoride |
| CF ₄ | Carbon tetrafluoride |
| CHF ₃ | Trifluormethane |
| CO ₂ | Carbon dioxide |
| H ₂ | Hydrogen |
| N ₂ | Nitrogen |
| N ₂ O | Nitrous oxide |

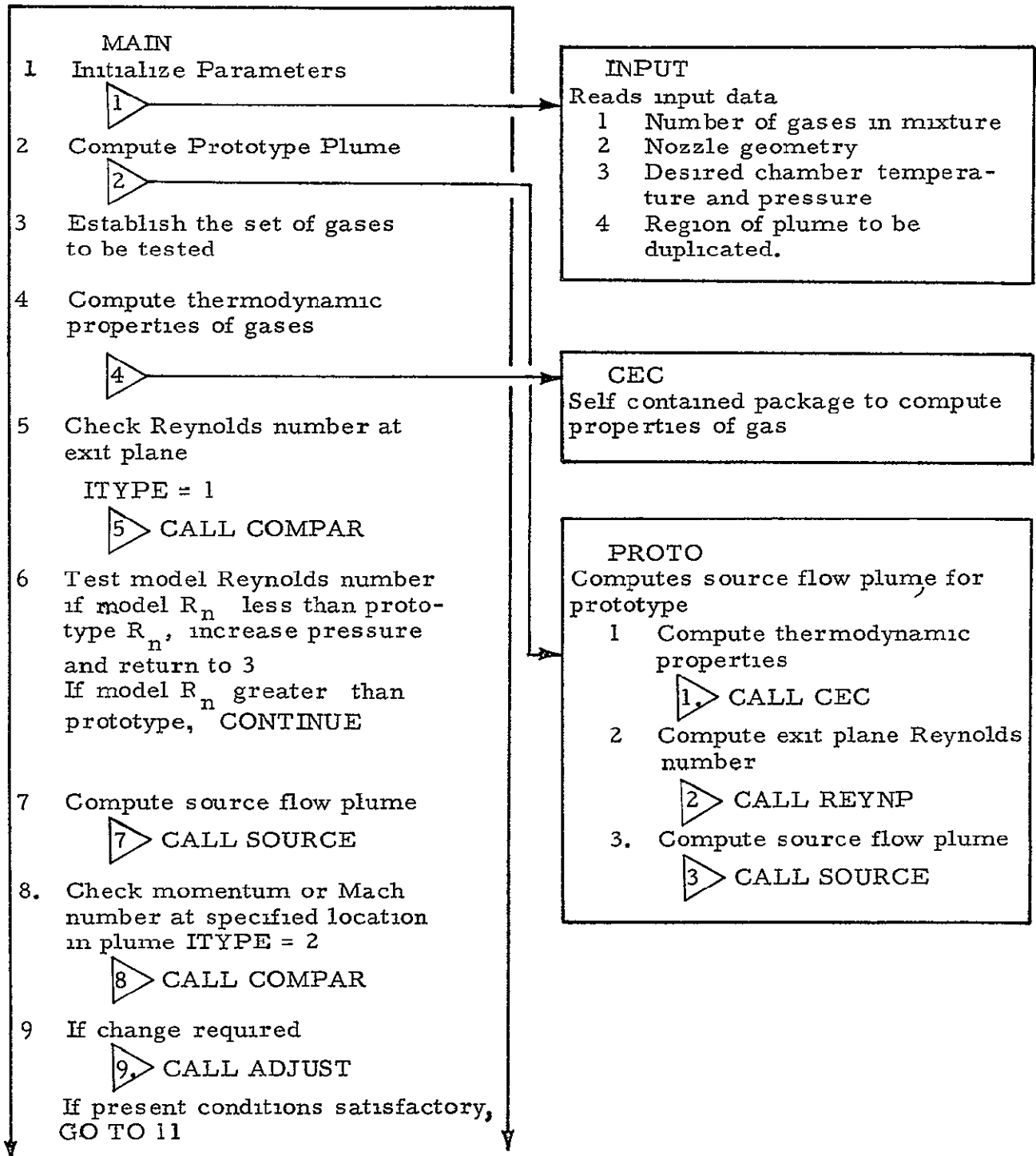


Fig C-1 — General Flow of Program

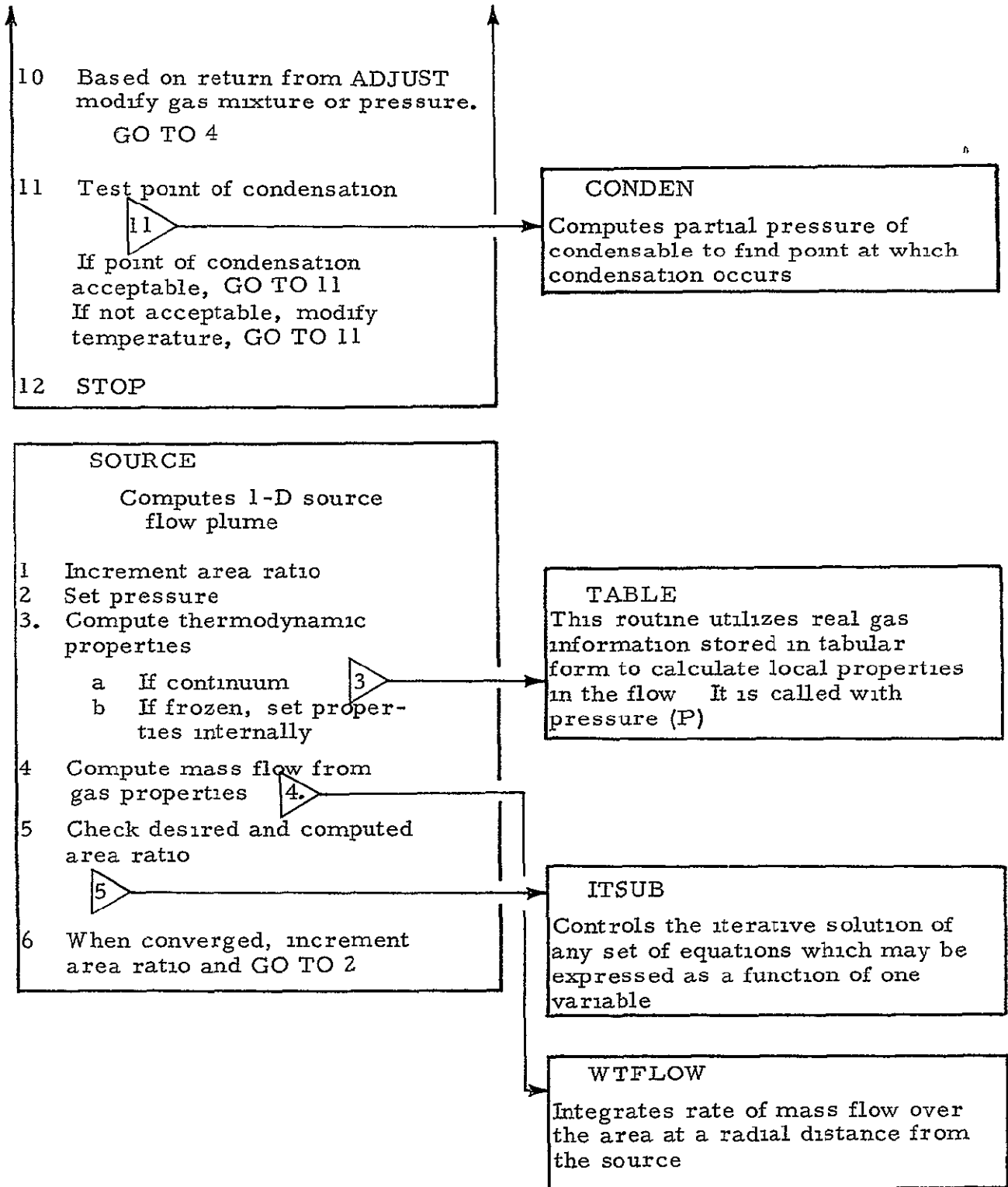


Fig C-1 Contd

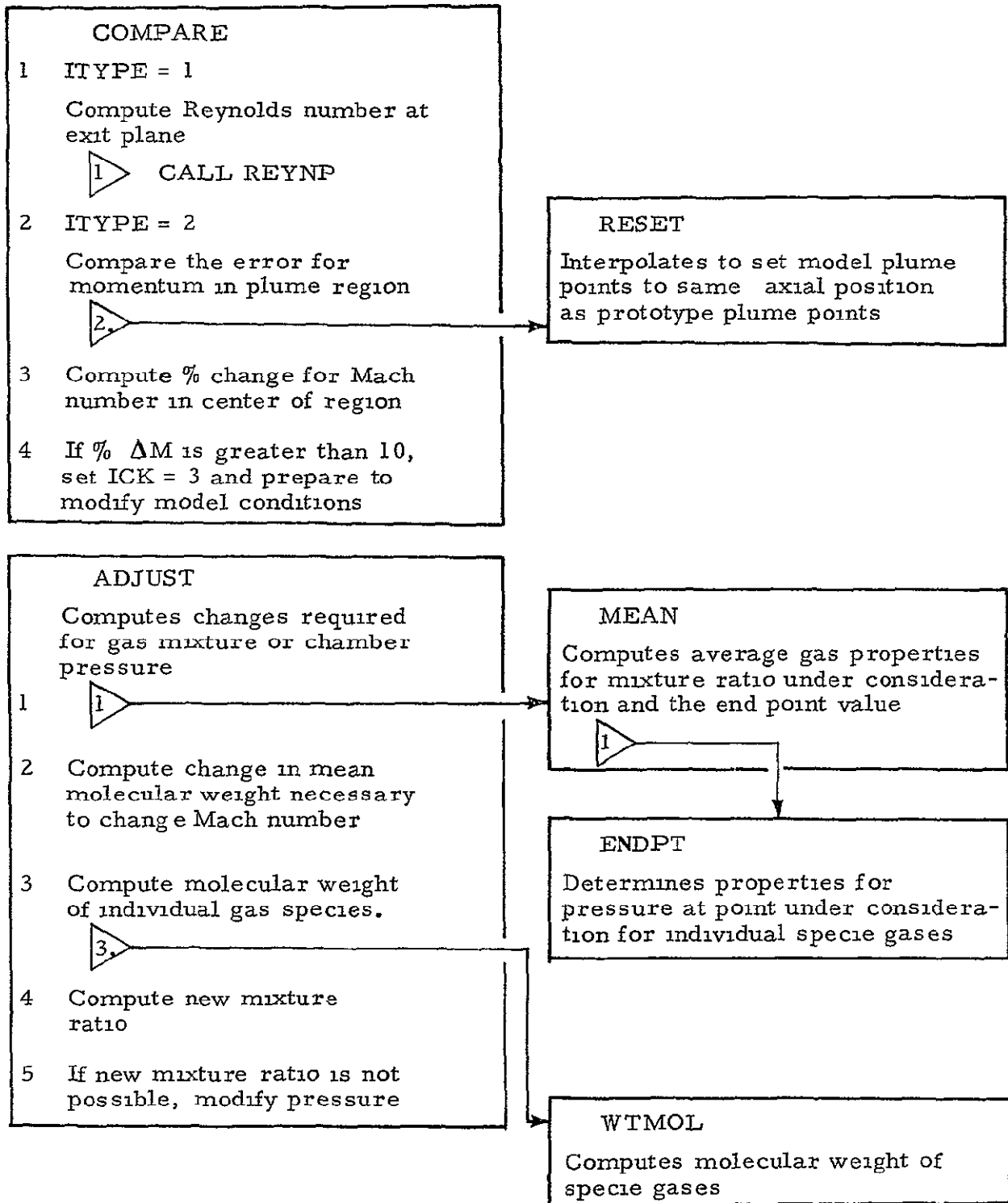


Fig. C-1 Contd

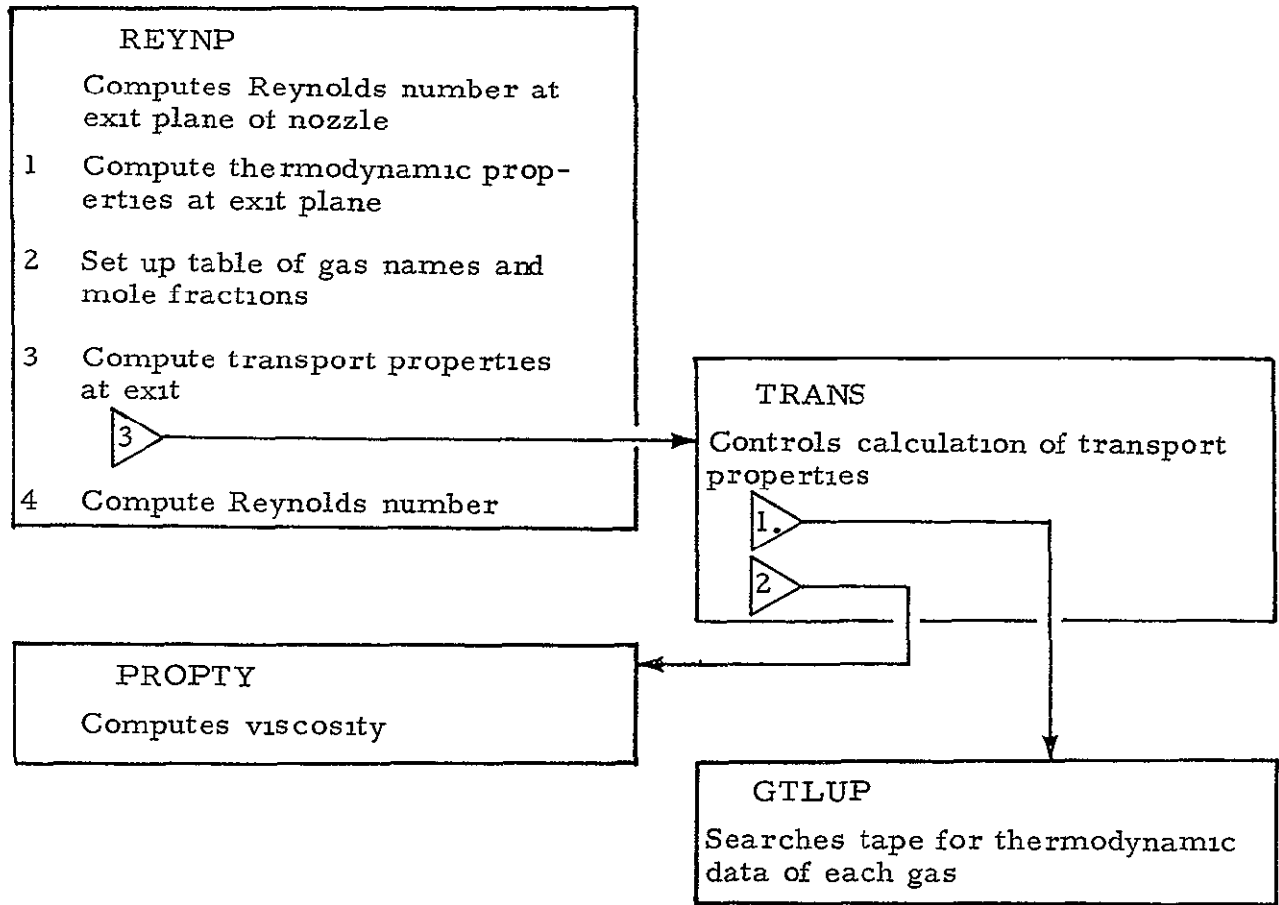


Fig C-1 Contd

C-7

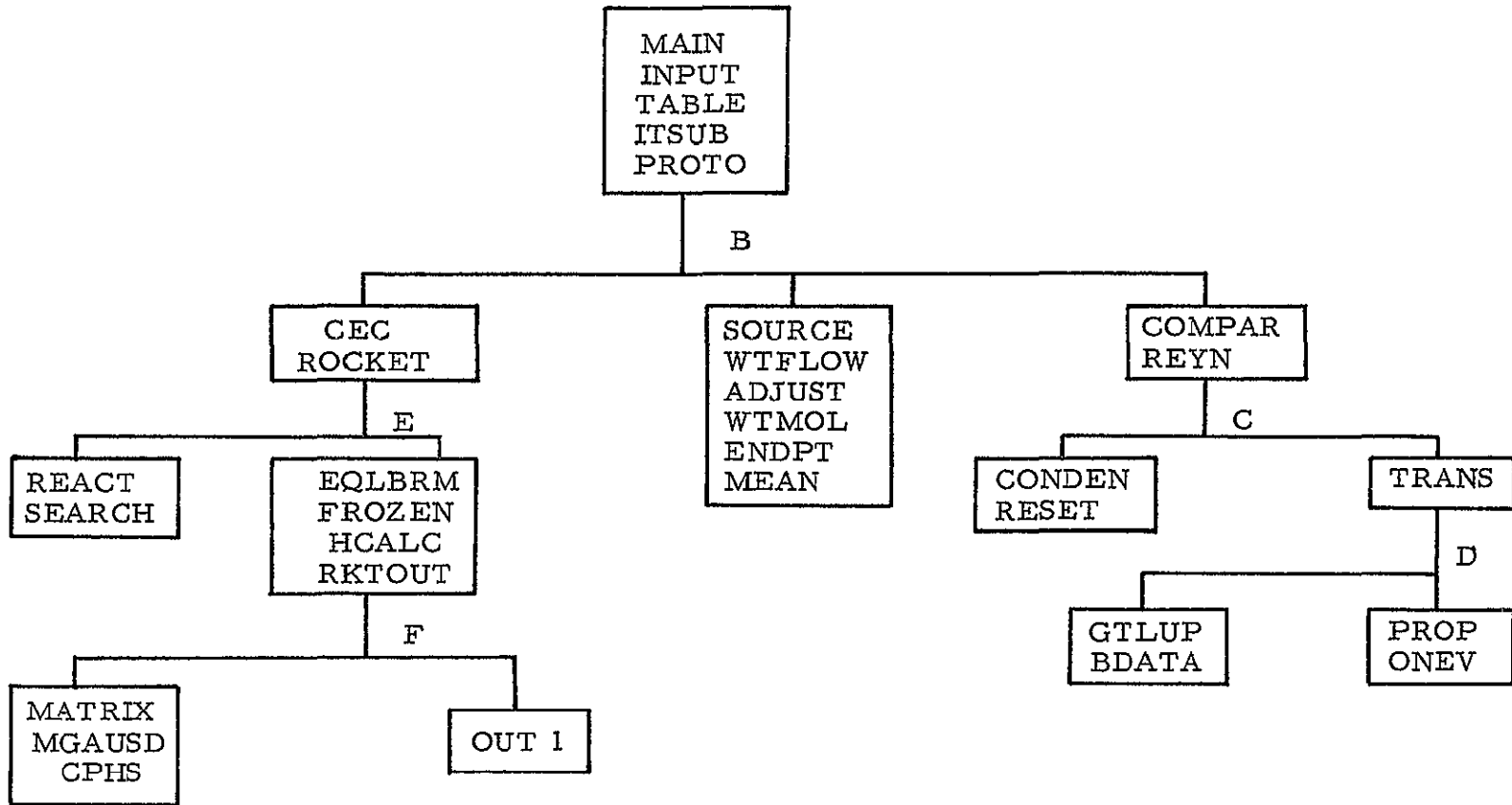


Fig C-2 -- Overlay Structure of Simulant Selection Program

C 2 1

INPUT GUIDE

| | | |
|--------------|---------|---|
| CARD NO 1 | | Problem Title or Identification |
| FORMAT | 12A6 | |
| Cols 1 - 72 | HOL | Comment card or header information |
| CARD NO 2 | Control | Card |
| FORMAT | 8I5 | |
| Cols 1 - 5 | NMIX | Number of gases to be used in simulant mixture |
| Cols 6 - 10 | NPTS | Number of points in plume to be matched Must be 3 |
| Col 11 - 15 | IP | 0 Set initial chamber pressure in program 1 Read in initial chamber pressure |
| Col 16 - 20 | IT | 0 Set initial chamber temperature in program 1 Read in initial chamber temperature |
| Col 21 - 25 | IG | 0 Gases to be selected by program 1 Specific gas mixture to be read in |
| Col. 26 - 30 | IFLAG | 0 Regular output 1 Intermediate output for debugging model information |
| Col 31 - 35 | ITYPE | 1 Calculation of simulation ability to be based on momentum flux comparison 2 Calculation of simulation ability to be based on Mach number comparison 3 Calculation of simulation ability to be based on Reynolds number comparison |
| CARD NO 3 | | |
| FORMAT | 7E10 6 | |

| | | |
|-------------|-----------------------------|--|
| Col 1 - 10 | ATM | Nossle throat area of model |
| Col 11 - 20 | RADTHM | Throat radius of model (ft) |
| Col 21 - 30 | AEOATM | Ratio of exit plane area to throat area of model |
| Col 31 - 40 | ANGLPM | Angle at nozzle lip of model (deg) |
| CARD NO 4 | | (Included if either chamber pressure or temperature is to be specified) |
| FORMAT | | 7E10 6 |
| Col 1 - 10 | PCHAMI | Model chamber pressure to be initially used Blank if not applicable (PSI) |
| Col 11 - 20 | TCHAMI | Model chamber temperature to be initially used Blank if not applicable (deg R) |
| CARD NO 5 | Prototype | Information |
| FORMAT | | 7E10 6 |
| Col 1 - 10 | RADP | Throat radius of prototype nozzle |
| Col 11 - 20 | AETP | Ratio of exit plane area to throat area for prototype |
| Col 21 - 30 | ANGP | Angle at exit plane of prototype nozzle (deg) |
| Col 31 - 40 | PREP | Chamber pressure of prototype (PSI) |
| CARDS No 6 | Prototype Fuel and Oxidizer | Information |
| FORMAT | | 5(A2, F7 0), 1X, A1, 1X, A1, 1X, 3E10 3 |
| Col 1 - 45 | PNAME | Fuel or oxidizer name (Products must be on CEC products tape) |
| Col 47 | LOF | F In col. 48 denotes fuel O In col. 48 denotes oxidizer |
| Col 49 | PHAZ | Phase of propellant L - Liquid G - Gas |
| Col 51 - 60 | WTFRAC | Weight fraction of fuel or oxidizer |
| Col 61 - 70 | HENTH | Heat of formation (in cal) of fuel or oxidizer |

| | | |
|--------------|----------------------|---|
| Col. 71 - 80 | HTEMP | Temperature (°K) associated with heat of formation |
| CARD NO 7 | Region of Simulation | |
| FORMAT | 7E10 6 | |
| Col 1 - 10 | XP11 | Axial location of point nearest nozzle in region of plume to be simulated (X/D from nozzle) |
| Col 11 - 20 | XP12 | Axial location of central point in simulated region (X/D from nozzle) |
| Col 21 - 30 | XP13 | Axial location of rear point in simulated region (X/D from nozzle) (XP11, XP12, XP13) |
| Col 31 - 40 | ERRMAX | Multiplication factor which may be input to modify the allowable percentage error used in the program. This allowable error is 10% and thus ERRMAX may be used to tighten or loosen this criteria ($0 < \text{ERRMAX}$) |

C 2.2 Description of Program Output

The simulant selection program output is organized into several basic groups which are easily recognizable. The initial output consists of input data. Thermodynamic data from the CEC portion of the program is then printed out. The next area contains data from calculations for the Reynolds number. Finally, a source flow plume is printed out. If this plume does not satisfy the required conditions a message is written out and further calculations are performed with output similar to that above. Detailed explanations are listed below. Numbered flags on the example output correspond to the numbered comments. Only pertinent output pages are shown.

Group I - Identification

(1) Title Identifies particular run.

Group II - Run Control

(2) Run Control Parameters These five parameters control program execution according to options selected. (See input guide for explanation of individual parameters.)

Group III - Model Nozzle Information

- (3) Model Nozzle Geometry These parameters are input and are explained in the input guide
- (4) Chamber Conditions Chamber temperature and pressure are either input or set by program as determined by Group I parameters

Group IV - Prototype Nozzle Information

- (5) Prototype Nozzle Geometry These parameters are input and are explained in the input guide

Group V - Plume Region Information

- (6) Plume Region These parameters define a region of the plume to be duplicated They are explained in the input guide
- (7) ERRMAX Described in input guide

Group VI - Prototype Gas Thermodynamic Information

This data is generated by the CEC portion of the program and contains data for an equilibrium combustion of the reactants and a frozen expansion of the products

- (8) Gas Data This page contains the thermodynamic data for the prototype engine The tables are self-explanatory (Units are on output)
- (9) This table contains gas parameters pertinent to the calculations of a source flow plume. This is the TAB array of the program

Group VIII - Prototype Reynolds Number Calculation

- (10) Prototype Reynolds Number

Group IX - Prototype Plume

- (11) Origin of source flow with respect to exit plane of nozzle - (ft)
- (12) Expansion angle of flow at nozzle lip - (radians)
- (13) Radial distance from source - (ft)
- (14) Mach number - Local Mach number
- (15) Reynolds number - Local Reynolds number
- (16) Gamma - specific heat ratio
- (17) Knudsen Number
- (18) Stagnation temperature - (^oR)
- (19) Static temperature - (^oR)
- (20) Stagnation pressure - (psf)
- (21) Static pressure - (psf)
- (22) Condensation point of H₂O in prototype plume - (ft), ternary system only

Group X - Model Gas Mixture

- (23) This data is computed by CEC portion of program. The tables are self-explanatory
- (24) This table contains gas parameters used in the calculation of a source flow plume This is the TAB array
- (25) } Gas data for individual species of gases in the simulant mixture Used
- (26) } in subsequent calculations (appear only when new gases or new chamber stagnation conditions are tried)

Group XI - Model Reynolds Number

This section contains exit plane properties and Reynolds number for model nozzle See Group VIII for explanation

Group XII Model Plume

Source flow plume for model nozzle See Group IX for explanation

C 3 SAMPLE IBM 7094 INSTRUCTION CARD

This sample card is included in the program direction to aid the user in running the program. Naturally this format will vary from machine to machine. The important data to note however, are the tape numbers and logic. These contain the data necessary for the calculation of thermodynamic and transport properties of many gases. See Refs 16 and 17.

- (1) Programmer name
- (2) Operation code - 11-production
- (3) Bin number - assigned by computer services
- (4) Location - Return completed job to this area
- (5) Job number - assigned by computer services
- (6) Simulation gases products tape
- (7) Transport property products tape
- (8) Complete products tape for CEC (Used in prototype calculations)
- (9) Time assigned by programmer (Usually 30 minutes of 7094 will suffice)
- (10) Number of lines assigned by programmer (Usually 15,000 will suffice)

| 7094- _____ INSTRUCTIONS | | | | | | | | | |
|--|-----------|--|-------------|------------|-----------------------|---------|---------------|--|------|
| NAME (1) | | | OP CODE (2) | | STACK # _____ | | | | |
| BIN # (3) | | LOC (4) | | JOB # (5) | | | | | |
| IF EXCEEDS MAX (15) | | | | | FAST TAPES A B C D | | | | |
| <input type="checkbox"/> STR <input type="checkbox"/> STE <input type="checkbox"/> DMP <input checked="" type="checkbox"/> RETSY | | | | | INPUT TAPES | | | WORK LOGIC | |
| (12-13) | | | | | LOGIC | REEL NO | DEN | | |
| <input checked="" type="checkbox"/> BSYS (11) | | <input checked="" type="checkbox"/> COMPL / ASSMBL (6) | | A 5 | | 2814 | | | |
| <input type="checkbox"/> SPOOR | | <input checked="" type="checkbox"/> EXECUTE | | A 7 | | 4640 | | | |
| <input type="checkbox"/> OTHER | | <input type="checkbox"/> PUNCH (BCD BIN) | | A 8 | | 4 451 | | | |
| <input checked="" type="checkbox"/> FTRN (14) | | <input type="checkbox"/> MAP | | | | | | | |
| <input type="checkbox"/> FTRN | | <input type="checkbox"/> FAP | | | | | | | |
| <input type="checkbox"/> APT | | <input type="checkbox"/> SCAT | | | | | | | |
| <input type="checkbox"/> PERT | | <input type="checkbox"/> OTHER | | | | | | | |
| LINES OF OUTPUT (1000S) (10) | | | | | MAXIMUM TIME (9) | | | | |
| <input type="checkbox"/> 0-5 <input type="checkbox"/> 5-15 <input type="checkbox"/> 15-30 <input type="checkbox"/> OVER | | | | | HOURS _____ | | MINUTES _____ | | |
| PROGRAMMER COMMENTS | | | | | NUMBER OF CASES _____ | | | | |
| OVER _____ | | | | | | | | | |
| OPERATOR COMMENTS | | | | | | | | <input type="checkbox"/> SEE ON LINE <input type="checkbox"/> SEE TECHNIQUE <input type="checkbox"/> MAX EXCEEDED <input type="checkbox"/> RETURN TO SYS <input type="checkbox"/> LINE MAX | |
| OPER INIT _____ OVER _____ | | | | | | | | | |
| OUTPUT TAPES ONLY | | | | | | | | | 4020 |
| REEL NO | LOGIC | DEN | UNIT | NO OF CPYS | SAVE | TAPE | | | |
| | B-1 | 8 | | | | | | | |
| | | | | | | | | | |
| | | | | | | | | | |
| | | | | | | | | | |
| | | | | | | | | | |
| | | | | | | | | | |
| | | | | | | | | | |
| NO FILES | NO FRAMES | COPIES | DENSITY | COPIY FLO | KALVAR | | | | |
| | | P F | 5 8 | P F | | | | | |
| | | | | | | | | | |

- (11) Job will be executed under IBM 7094 IBSYS system
- (12) Computer is to compile and assemble the subroutines in binary form suitable for execution
- (13) After compilation and loading of the binary form of the subroutines the program is to be executed
- (14) The program coding is in FORTRAN IV language
- (15) If either maximum time or maximum pages exceeded, the program control is to be returned to the IBSYS system and the job terminated

If the dump is checked and either of the above occurs, the computer operator will initiate a dump of the program and the variables stored in the core

Appendix D

PROGRAM LISTING AND PRINTOUT

```

$JOB          H029-LMSC L5207      ,911000,00,12,I40CEP
*           DATE      MAY 70      SEQ= G602
$EXECUTE      IBJOB
$IBJOB        MAP,LOGIC,GO,FIOCS,SOURCE,FLOW
$IBFTC MAIN
C      CONTROLLING PROGRAM
C      SETS INPUT ANDS CALLS CEC
C      TO LESSEN THE NO. OF CHANGES THAT MUST BE MADE, THE THERMODYNAMIC
C      DATA FOR THE TRANSPORT PROPERTIES WILL BE READ FROM TAPE 12, THE
C      OLD NASA/LEWIS DATA TAPE.
C      THE THERMODYNAMIC DATA FOR THE CEC PORTION WILL BE READ FROM TAPE
C      4, THE NEW DATA TAPE GENERATED BY MCDERMIT.
C      TO MAKE THESE COMPATABLE THE CEC IS MODIFIED TO READ THE GAS NAME
C      UNDER A 2A6 FORMAT.
COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
COMMON/PLUMF1/PRPR(10,4),REYPLM
COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DEL,DELMN,
$DELREY
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/GASES/TAB(3,12,13),NMIX
COMMON/GASFO/GASNAM(10,5,4),GNUM(10,5,4),NML(10,4),
1FZG(10,4),FXG(10,4),ENTHG(10,4),RTEMPG(10,4)
COMMON/SUNUP/SUN(3,40,2)
COMMON/CHAMB/PCHAMI,TCHAMI,PMAX,TMAX
COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
INTEGER GASNAM
COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
COMMON/LIP/THET,PI02
COMMON/EXCON/PEX,EMU
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4,RHOP,RMW(15),TLN
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2,TOTN(13)
COMMON/COUNT/IKLUG

```

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```

COMMON/WRIT/IFLG1
COMMON/TAPE/IPROT
COMMON/MOLFRC/ZFRAC(40),KFR
  COMMON/PNT/KPT(4)
DATA LANK/1H /
COMMON/MGEOM/ATM,RADTHM,AEOATM,ANGLPM
COMMON/MOLWT/SA,SB,SC
DIMENSION PSI(10,4)
LOGICAL KAZE
C   IRNK IS COUNTER IF MIXTURE CHANGES FOR REYNOLDS NO. CALC
  IRNK=0
  IKLUG=0
C   READ INPUT INFO AND SET GAS DATA
  CALL INPUT
  PCMAX=.5
  PI=3.14159
  P02=PI/2.0
C
C   CALL PROTO
C   RESET GEOMETRY VALUES TO THOSE OF MODEL
  RADTHT=RADTHM
  AEOAT= AEOATM
  ANGLP= ANGLPM
  AT=ATM
C   USE CEMDAT TO SET UP POSSIBLE SIMULANT GAS NAMES
C   SET UP A STANDARD ARRAY TO CONTAIN POSSIBLE SIMULANT GAS DATA
C   LAST DIGIT DESIGNATES THE CATAGORY TO WHICH THE GAS BELONG
C   1 IS LOW-GAMMA GAS,2 IS HI-GAMMA GAS
C   3 IS CONDENSABLE
C   FIRST DICIT COUNTS NO. OF GASES IN CATAGORY
C   SECOND DIGIT INDICATES ELEMENT IN GAS TYPE
C   NEED TO LOAD IN REF. TEMP. AND ENTHALPY
  RTEMPG(1,2)=298.15
  ENTHG(1,2) =0.0
  RTEMPG(2,2)=298.15
  ENTHG(2,2) =0.0
  RTEMPG(3,2)=298.15
  ENTHG(3,2) =0.0

```

```
RTEMPG(4,2)=298.15
ENTHG(4,2) =19490.0
RTEMPG(1,1)=298.15
ENTHG(1,1) --217200.0
PTEMPG(2,1)= 298.15
ENTHG(2,1) =-162600.0
RTEMPG(1,3)=298.15
ENTHG(1,3) =-94051.8
RTEMPG(2,3)=298.15
ENTHG(2,3) =-171900.0
PSI(1,1)=88.
PSI(2,1)=71.
PSI(1,2)=28.
PSI(2,2)=39.9
PSI(3,2)=2.
PSI(4,2)=44.
PSI(1,3)=44.
PSI(2,3)=106.4
```

```
C INITIALIZE GUESS OF MIXTURE RATIO
```

```
PC11=1.0
PC21=0.5
PC22=0.5
PC31=0.4
PC32=0.4
PC33=0.2
DP3=.05
```

```
PHOLD=PCHAMI
THOLD=TCHAMI
```

```
C THIS SECTION INTIALIZES THE GAS SELECTION PROCEDURE
```

```
C L IS COUNTER ON CONDENSABLE
```

```
L=1
```

```
C KAZE IS SET FALSE IF MIXTURE IS CHANGED
```

```
KAZE =.TRUE.
```

```
KASE=0
```

```
IRNT=0
```

```
IF(IG.EQ.1)GO TO 400
```

```
K=1
```

```
C EVENTUALLY A SYSTEM WILL BE SET UP TO SELECT SINGLE GAS
```

```

C      THAT APPROXIMATES A PT IN THE FIELD
      IF(NMIX.EQ.3)GO TO 200
      IF(NMIX.GT.1)GO TO 100
15  I=0
20  I=I+1
31  CONTINUE
      DO 11 J=1,5
      NAME(1,J)=GASNAM(I,J,K)
11  ANUM(1,J)=GNUM(I,J,K)
      ENTH(1)=ENTHG(I,K)
      RTEMP(1)=RTEMPG(I,K)
      FAZ(1)=FZG(I,K)
      FOX(1)=FXG(I,K)
      PECWT(1)=PC11
      P=PHOLD
      T=THOLD
      NAME(2,1)=LANK
C
C      GO TO 400 ,CALL CEC FOR 1 GAS
      GO TO 400
100 CONTINUE
      IT1=0
21  IT1=IT1+1
33  CONTINUE
      DO 12 J=1,5
      NAME(1,J)=GASNAM(IT1,J,1)
12  ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1)=ENTHG(IT1,1)
      RTEMP(1)=RTEMPG(IT1,1)
      FAZ(1)=FZG(IT1,1)
      FOX(1)=FXG(IT1,1)
      SA = PSI(IT1,1)
      PECWT(1)=PC21
C
      IF(1RNK.EQ.1)GO TO 34
      IT2=0
22  IT2=IT2+1
34  CONTINUE

```



```

DO 13 J=1,5
SB = PSI(IT2,2)
NAME(2,J)=GASNAM(IT2,J,2)
13 ANUM(2,J)=GNUM(IT2,J,2)
ENTH(2)=ENTHG(IT2,2)
RTEMP(2)=RTEMPG(IT2,2)
FAZ(2)=FZG(IT2,2)
FOX(2)=FXG(IT2,2)
PECWT(2)=PC22
P=PHOLD
T=THOLD
C
NAME(3,1)=LANK
C GO TO 400,CALL CEC FOR 2 GASES
GO TO 400
200 CONTINUE
C INITIALIZE FOR TERNARY, USE CO2 FOR CONDENSABLE
IT1=0
23 IT1=IT1+1
35 CONTINUE
DO 14 J=1,5
NAME(1,J)=GASNAM(IT1,J,1)
14 ANUM(1,J)=GNUM(IT1,J,1)
ENTH(1)=ENTHG(IT1,1)
RTEMP(1)=RTEMPG(IT1,1)
FAZ(1)=FZG(IT1,1)
FOX(1)=FXG(IT1,1)
SA = PSI(IT1,1)
PECWT(1)=PC31
C
IF(IRNK.EQ.1)GO TO 36
IT2=0
24 IT2=IT2+1
36 CONTINUE
DO 85 J=1,5
NAME(2,J)=GASNAM(IT2,J,2)
85 ANUM(2,J)=GNUM(IT2,J,2)
ENTH(2)=ENTHG(IT2,2)

```

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```

RTEMP(2)=RTEMPG(IT2,2)
FAZ(2)=FZG(IT2,2)
FOX(2)=FXG(IT2,2)
SB = PSI(IT2,2)
PECWT(2)=PC32
C SET CONDENSABLE CO2
DO 16 J=1,5
NAME(3,J)=GASNAM(L,J,3)
16 ANUM(3,J)=GNUM(L,J,3)
ENTH(3)=ENTHG(L,3)
RTEMP(3)=RTEMPG(L,3)
FAZ(3)=FZG(L,3)
FOX(3)=FXG(L,3)
SC = PSI(L,3)
PECWT(3)=PC33
P=PHOLD
T=THOLD
NAME(4,1)=LANK
400 CONTINUE
KASE=KASE+1
WRITE(6,41)
41 FORMAT(30X,31HGAS MIXTURE UNDER CONSIDERATION//35X,4HNAME,15X,
113HMIXTURE RATIO)
DO 42 MC=1,NMIX
WRITE(6,44)(NAME(MC,IC),ANUM(MC,IC),IC=1,5),PECWT(MC)
44 FORMAT(15X,5(A2,1X,F7.4,2X),5X,F7.4)
42 CONTINUE
CALL CEC(1,KASE)
WRITE(6,310)
310 FORMAT(1H1)
WRITE(6,51)
51 FORMAT(40X,45HTABLE OF THERMODYNAMIC PROPERTIES FOR MIXTURE)
WRITE(6,52)
52 FORMAT(15X,8HH FT2/S2,5X,4HA/A*,7X,5HGAMMA,6X,5HM NO.,10X,5HP PSF,
16X,7HT DEG R,5X,6HMOL WT)
NPT=KPT(1)
WRITE(6,53)(( TAB(1,I,J),I=1,7),J=1,NPT)
53 FORMAT(13X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X)

```

```

      $E10.3)
C     TEST IF MIXTURE GASES HAVE CHANGED
      IF(.NOT.FAZE)GO TO 801
C     NOW DETERMINE ENDPTS. OF MIXTURE
      IF(NMIX.EQ.1)GO TO 500
      IF(NMIX.EQ.2)GO TO 550
      IF(NMIX.EQ.3)GO TO 600
500  IF(I.GE.IG1)GO TO 510
      GO TO 20
510  IF(K.EQ.4)GO TO 1000
      K=K+1
      GO TO 15
550  CONTINUE
      PECWT(1)=1.0
      NAME(2,1)=LANK
      P=PHOLD
      T=THOLD
      CALL CEC(2,KASE)
      DO 551 J=1,5
      NAME(1,J)=GASNAM(IT2,J,2)
551  ANUM(1,J)=GNUM(IT2,J,2)
      RTEMP(1)=RTEMPG(IT2,2)
      ENTH(1)= ENTHG(IT2,2)
      FAZ(1) = FZG(IT2,2)
      FOX(1) = FXG(IT2,2)
      P=PHOLD
      T=THOLD
      CALL CEC(3,KASE)
C     AFTER CEC COMPUTES ENDPTS.,THE GAS NAMES MUST BE RESET
580  DO 552 J=1,5
      NAME(1,J)=GASNAM(IT1,J,1)
552  ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1) = ENTHG(IT1,1)
      RTEMP(1) =RTEMPG(IT1,1)
      FAZ(1)   =FZG(IT1,1)
      FOX(1)   =FXG(IT1,1)
      DO 553 J=1,5
      NAME(2,J)=GASNAM(IT2,J,2)

```

```

553 ANUM(2,J)=GNUM(IT2,J,2)
    ENTH(2) =ENTHG(IT2,2)
    RTEMP(2) =RTEMPG(IT2,2)
    FAZ(2) =FZG(IT2,2)
    FOX(2) =FXG(IT2,2)
    PECWT(1)=PC21
    PECWT(2)=PC22
    NAME(3,1)=LANK
C    GAS PROPERTIES LOADED INTO TAB ARRAY,1-MIXTURE,2-ENDPT,3-ENDPT
    GO TO 800
600 CONTINUE
C    NOW TO SET ENDPTS FOR TERNARY MIXTURE
    DO 554 J=1,5
    NAME(2,J)=GASNAM(L,J,3)
554 ANUM(2,J)=GNUM(L,J,3)
    ENTH(2) =ENTHG(L,3)
    RTEMP(2) =RTEMPG(L,3)
    FAZ(2) =FZG(L,3)
    FOX(2) =FXG(L,3)
    NAME(3,1)=LANK
    PECWT(1) =PC31+PC32
    PECWT(2) =PC33
    P=PHOLD
    T=THOLD
    CALL CEC(2,KASE)
    DO 555 J=1,5
    NAME(1,J)=GASNAM(IT2,J,2)
555 ANUM(1,J)=GNUM(IT2,J,2)
    ENTH(1) =ENTHG(IT2,2)
    RTEMP(1) =RTEMPG(IT2,2)
    FAZ(1) =FZG(IT2,2)
    FOX(1) =FXG(IT2,2)
    P=PHOLD
    T=THOLD
    CALL CEC(3,KASE)
C    AFTER TERNARY ENDPTS COMPUTED, RESET GASES
    PECWT(1)=PC31
    PECWT(2)=PC32

```

```

      DO 557 J=1,5
      NAME(1,J)=GASNAM(IT1,J,1)
557 ANUM(1,J)=GNUM(IT1,J,1)
      ENTH(1) =ENTHG(IT1,1)
      RTEMP(1) =RTEMPG(IT1,1)
      FAZ(1)   =FZG(IT1,1)
      FOX(1)   =FXG(IT1,1)
      DO 558 J=1,5
      NAME(2,J)=GASNAM(IT2,J,2)
558 ANUM(2,J)=GNUM(IT2,J,2)
      ENTH(2) =ENTHG(IT2,2)
      RTEMP(2) =RTEMPG(IT2,2)
      FAZ(2)   =FZG(IT2,2)
      FOX(2)   =FXG(IT2,2)
      DO 559 J=1,5
      NAME(3,J)=GASNAM(L,J,3)
559 ANUM(3,J)=GNUM(L,J,3)
      ENTH(3) =ENTHG(L,3)
      RTEMP(3) =RTEMPG(L,3)
      FAZ(3)   =FZG(L,3)
      FOX(3)   =FXG(L,3)
      NAME(4,1)=LANK
C
800 CONTINUE
      WRITE(6,310)
      WRITE(6,61)
      61 FORMAT(40X,49HTABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 1)
      WRITE(6,52)
      NPT=KPT(2)
      WRITE(6,53)(( TAB(2,I,J),I=1,7),J=1,NPT)
      WRITE(6,310)
      WRITE(6,71)
      71 FORMAT(40X,49HTABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 2)
      WRITE(6,52)
      NPT=KPT(3)
      WRITE(6,53)(( TAB(3,I,J),I=1,7),J=1,NPT)
801 CONTINUE
C

```

```

C      COMPARE RN AT EXIT PLANE
      CALL COMPAR (1,IOK,IRCON,KASE)
      IRNK=0
      IF(IRNT.GE.1) GO TO 802
      IF(IRCON.EQ.1)GOTO1100
      IF(IOK.GT.1)GO TO 900
C      COMPUTE SOURCE FLOW PLUME
802  CONTINUE
      IDZ=0
      CALL SOURCE(IDZ,ISCON)
      IF(ISCON.EQ.1)GO TO 1100
C      COMPARE PLUME REGION
      CALL COMPAR(2,IOK,IDUM,KASE)
      IF(IG.EQ.1)GO TO 1100
      IF(IOK.EQ.0)GO TO 1000
      CALL ADJUST(      NOK,KAZE)
      IF(NMIX.EQ.1.AND.NOK.EQ.0)GO TO 855
      IF(NMIX.EQ.1.AND.NOK.GT.0)GO TO 850
      IF(NMIX.EQ.2.AND.NOK.EQ.0)GO TO 865
      IF(NMIX.EQ.2.AND.NOK.GT.0)GO TO 860
      IF(NMIX.EQ.3.AND.NOK.EQ.0)GO TO 875
      IF(NMIX.EQ.3.AND.NOK.GT.0)GO TO 870
C      MODIFY GASES ACCORDING TO INPUT FROM ADJUST
850  THOLD=TNW
      PHOLD=PNW
      IRNK=0
      IF(I.LT.IG1)GO TO 20
      IF(I.GE.IG1)I=0
      K=2
      IF(I.GT.IG2)GO TO 1020
      GO TO 20
855  T=TNW
      P=PNW
      THOLD=TNW
      PHOLD=PNW
      GO TO 400
860  THOLD=TNW
      PHOLD=PNW

```

```
IRNK=0
PC21=.5
PC22=.5
IF(IT2.LT.IG2)GO TO 22
IF(IT1.LT.IG1)GO TO 21
GO TO 980
865 T=TNW
P=PNW
PHOLD=PNW
THOLD=TNW
PECWT(1)=PC21
PECWT(2)=PC22
GO TO 400
870 THOLD=TNW
PHOLD=PNW
IRNK=0
PC31 =.4
PC32=.4
PC33=.2
IF(IT2.LT.IG2)GO TO 24
IF(IT1.LT.IG1)GO TO 23
GO TO 985
875 T=TNW
P=PNW
THOLD=TNW
PHOLD=PNW
PECWT(1)=PC31
PECWT(2)=PC32
PECWT(3)=PC33
GO TO 400
980 WRITE(6,981)
981 FORMAT(5X,33HNO DESIRABLE BINARY MIXTURE FOUND)
WRITE(6,706)
706 FORMAT(20X,43HOTO ACHIEVE CONVERGENCE, INCREASE ERROR BAND)
GO TO 1100
985 WRITE(6,986)
986 FORMAT(5X,72HNO DESIRABLE TERNARY MIXTURE FOUND FOR PRESENT CONDEN
ISABLE RATIO, MODIFY)
```

```

WRITE(6,706)
PC33=PC33+DP3
PH=(1.0-PC33)/2.0
PC31=PH
PC21=PH
IF(PC33.LE.PCMAX)GO TO 200
WRITE(6,701)
701 FORMAT(5X,73HNO DESIRABLE TERNARY MIXTURE FOUND FOR PRESENT CONDE
2NSABLE, USE NEXT GAS)
PC33=.2
PC31=.4
PC32=.4
L=L+1
IF(L.LE.IG3)GO TO 200
WRITE(6,705)
705 FORMAT(41HNO MIXTURES FOUND FOR PRESENT CONDITIONS)
GO TO 1100
900 CONTINUE
C THIS SECTION INCREASES CHAMBER TEMPERATURE TO COMPENSATE FOR
C LOW REYNOLDS NO.
T =TCHAM1 + 300.
WRITE(6,967)
967 FORMAT(20X, 56HINCREASING CHAMBER TEMPERATURE TO RAISE REYNOLDS N
$UMBER)
P= PCHAM1
IRNT = IRNT+1
PHOLD=P
THOLD=T
IRNK=1
IF(NMIX.EQ.1)GO TO 31
IF(NMIX.EQ.2)GO TO 33
IF(NMIX.EQ.3)GO TO 35
1000 CONTINUE
IF(NMIX.EQ.2) GO TO 1100
WRITE(6,1001)
1001 FORMAT(73HOLAST COMPUTED MIXTURE ACCEPTABLE POINT OF CONDENSATION
*NOW BEING CHECKED)
ICON=L

```



```
CALL CONDEN(ICON,ISW,IACP,TONEW)
IF(ISW.EQ.0)GO TO 1010
IF(IACP.EQ.0)GO TO 1050
C TEMPERATURE CALCULATED IS UNACCEPTABLE, MODIFY GASES
NOK=1
PNW=PCHAMI
TNW=TCHAMI
GO TO 870
1050 NOK=0
PNW=P
TNW=TONEW
GO TO 875
1020 WRITE(6,1021)
1021 FORMAT(31HONO ACCEPTABLE SINGLE GAS FOUND)
1010 CONTINUE
1100 CONTINUE
STOP
END
```

```

$IBFTC INPUT DECK
SUBROUTINE INPUT
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1, TM, TLOW, TMID, THIGH, PP, CPSUM, OF, EQRAT, FPCT, R, RR, HSUBO, AC(2), AM(2)
2, HPP(2), RHO(2), VMIN(2), VPLS(2), WP(2), DATA(22), NAME(15,5)
3, ANUM(15,5), PECWT(15), ENTH(15), FAZ(15), RTEMP(15), FOX(15), DENS(15)
4, RHOP, RMW(15), TLN
COMMON/GASFO/GASNAM(10,5,4), GNUM(10,5,4), NML(10,4),
1FZG(10,4), FXG(10,4), ENTHG(10,4), RTEMPG(10,4)
COMMON/WRIT/IFLG1
COMMON/GEOM/AT, RADTHT, AEOAT, ANGLP, REYNP
COMMON/GASES/TAB(3,12,13), NMIX
COMMON/CHAMB/PCHAMI, TCHAMI, PMAX, TMAX
COMMON/NUMG/IG1, IG2, IG3, IG4, PCMAX, IG
COMMON/PROTG/PNAME(4,5), AOF(4), WTFRAC(2), PNUM(4,5), HENTH(4),
1HTEMP(4), PHAZ(4)
COMMON/REGION/XPI1, XPI2, XPI3, ERRMAX, ITYPE
COMMON/PROTN/RADP, AETP, ANGP, PREP
COMMON/MGEOM/ATM, RADTHM, AEOATM, ANGLPM
DIMENSION HEADER(12)
C READ NO. OF GASES DESIRED IN MIXTURE AND NO. OF AXIAL PTS IN PLUME
IG=0
READ(5,1)(HEADER(I), I=1,12)
1 FORMAT(12A6)
C HEADER IDENTIFIES PARTICULAR RUN
WRITE(6,100)
100 FORMAT(1H1)
WRITE(6,2)HEADER
2 FORMAT(30X,12A6)
READ(5,5)NMIX,NPTS,IP,IT,IG,IFLG1,ITYPE
5 FORMAT(8I5)
WRITE(6,7)NMIX,NPTS,IP,IT,IG,IFLG1,ITYPE
7 FORMAT(15X,5HNMIX=,15,5X,5HNPTS=,15,5X,3HIP=,15,5X,3HIT=,15,5X,
13HIG=,15,5X,6HIFLG1=,15,5X,6HITYPE=15)
TMAX=2000.
PMAX=1500.
IF(IP.EQ.0.AND.IT.EQ.0)GO TO 20
IF(IP.EQ.1.AND.IT.EQ.0)GO TO 10

```

```

      IF(IP.EQ.0.AND.IT.FQ.1)GO TO 15
C     READ BOTH INITIAL CHAMBER T AND P
      READ(5,6)PCHAMI,TCHAMI
      6 FORMAT(7E10.6)
      GO TO 30
      10 READ(5,6)PCHAMI
      GO TO 29
      15 READ(5,6)PDUM,TCHAMI
      20 PCHAMI=200.
      29 CONTINUE
      IF(IT.EQ.1)GO TO 30
      TCHAMI=1800.
      30 CONTINUE
C     READ GEOMETRY OF THROAT
      READ(5,6)ATM,RADTHM,AFOATM,ANGLPM
      WRITE(6,31)
      31 FORMAT(1H0///,40X,23HNOZZLE GEOMETRY FOLLOWS)
      WRITE(6,37)
      37 FORMAT(1H0,29X,11HTHROAT AREA,5X,13HTHROAT RADIUS,5X,10HAREA RATIO,
      $,5X,9HLIP ANGLE)
      WRITE(6,33)ATM,RADTHM,AEOATM,ANGLPM
      33 FORMAT(30X,6(E10.3,5X))
      TCHAMI=TCHAMI/1.8
      WRITE(6,91)TCHAMI,PCHAMI
      91 FORMAT(1H0//,30X,21HINITIAL CHAMBER TEMP=E10.3,5X,9HPRESSURE=E10.3
      1)
      READ(5,6)RADP,AETP,ANGP,PREP
      WRITE(6,110)
      110 FORMAT(1H0//,40X,21HPROTOTYPE INFORMATION)
      WRITE(6,120)RADP,AETP,ANGP,PREP
      120 FORMAT(30X,5HRADP=E10.3,5HAETP=E10.3,5HANGP=E10.3,5HPREP=E10.3)
      DO 140 I=1,2
      READ(5,130)(PNAME(I,J),PNUM(I,J),J=1,5),AOF(I),PHAZ(I),WTFRAC(I),
      $HENTH(I),HTEMP(I)
      140 CONTINUE
      130 FORMAT(5(A2,F7.0),1X,A1,1X,A1,1X,3E10.3)
C     ARE INITIAL GASES INPUT OR SELECTED BY PROGRAM
      IF(IG.EQ.0)GO TO 60

```

```

L=0
L=L+1
DO 50 N=1,NMIX
  READ(5,40)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),NML(N,L),ENTH(N),
1FAZ(N),RTEMP(N),FOX(N),DENS(N)
40 FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5)
50 CONTINUE
  WRITE(6,84)
84 FORMAT(40X,24HINPUT GAS FOR SINGLE RUN)
  DO 83 J=1,NMIX
    WRITE(6,81)(NAME(J,I),ANUM(N,I),I=1,5),PECWT(J),NML(J,L),ENTH(J),
1FAZ(J),RTEMP(J),FOX(N),DENS(N)
81 FORMAT(1X,5(A2,1X,F7.4,2X),F8.4,2X,A1,F11.2,2X,F8.3,2X,
1A1,3X,F8.5)
83 CONTINUE
60 CONTINUE
  READ(5,6)XPI1,XPI2,XPI3,ERRMAX
C  XPI1 AN XPI3 ARE AXIAL PTS. DEFINING REGION OF INTEREST
  WRITE(6,150)
150 FORMAT(1H0//,45X,32HREGION OF PLUME TO BE DUPLICATED)
  WRITE(6,160)XPI1,XPI2,XPI3
160 FORMAT(35X,4HXP1=E10.3,2X,4HXP2=E10.3,2X,4HXP3=E10.3)
  WRITE(6,170)ERRMAX
170 FORMAT(1H0///,30X,30HERROR MULTIPLICATION FACTOR = E10.3)
  RETURN
  END

```

```

$IBFTC TABL1  DECK
      SUBROUTINE TABLE (P,I1)
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/PNT/KPT(4)
      COMMON/GASCON/GAMA,R,T0,P0,EM,RHC,T,WM ,Q
      COMMON/EI TH/H
C     IL IS THE NO. OF PRESSURE CUTS
      IL=KPT(I1)
      EQUIVALENCE(NPT ,IL)
      UGC=1545.
      I=11
      RGC=UGC/TAB(I,7,IL)*32.174
      PP=P
      IF(PP.LT.TAB(I,5,IL))PP=TAB(I,5,IL)
      IF(PP.GT.TAB(I,5,1))PP=TAB(I,5,1)
      IF(P.LT.TAB(I,5,IL).OR.P.GT.TAB(I,5,1))GO TO 50
      IT=0
5     IT=IT+1
      IF(PP.LE.TAB(I,5,IT))GO TO 5
      IT=IT-1
      HP=(PP-TAB(I,5,IT))/(TAB(I,5,IT+1)-TAB(I,5,IT))
      GAMA= TAB(1,3,IT) +HP*(TAB(1,3,IT+1)-TAB(1,3,IT))
      XSIP=ALOG(TAB(I,5,IT)/TAB(I,5,IT+1))/ALOG(TAB(I,6,IT)/TAB(I,6,IT+
1))
      ONOX=1./XSIP
      T=(PP/TAB(I,5,IT))*ONOX*TAB(I,6,IT)
C     COMPUTE CP
      XSIH=(TAB(1,1,IT+1)-TAB(1,1,IT))/(TAB(1,6,IT+1)-TAB(1,6,IT))
      H=TAB(1,1,IT)+XSIH*(T-TAB(1,6,IT))
      H0=TAB(1,1,1)
      Q=SQRT(2.*ABS(H0-H))*(H0-H)/ABS(H0-H)
      QSQ=Q**2
      R=RGC
      A=SQRT(GAMA*R*T)
      EM=Q/A
      T0= T+ (GAMA-1.)*QSQ/(2.*GAMA*RGC)
      P0= PP*(T0/T)**(GAMA/(GAMA-1.))
      WM= TAB(I,7,IT)

```

```

      RHO= PP/(RGC*T) *32.174
      GO TO 100
50  CONTINUE
C   COMPUTATION IF P OUTSIDE TABLE
      IF(P.GT.TAB(I,5,1))GO TO 70
      IF(P.LT.TAB(I,5,IL))GO TO 80
70  T1=TAB(I,6,1)
      GAMA=TAB(I,3,1)
      H1=TAB(I,1,1)
      GO TO 90
80  T1=TAB(I,6,IL)
      GAMA=TAB(I,3,IL)
      H1=TAB(I,1,IL)
90  CONTINUE
      T=T1*(P/PP)**((GAMA-1.)/GAMA)
      A=SQRT(GAMA*RGC*T)
C   TAB(I,1,IP) WILL CONTAIN ENTHALPY
C   XSIH IS CP
      XSIH=GAMA*RGC/(GAMA-1.)
      H=H1+XSIH*(T-T1)
      H0=TAB(I,1,1)
      Q=SQRT(2.*(H0-H))
      RHO= P/(T*RGC)*32.174
      EM = Q/A
      WM=TAB(I,7,1)
      R=RGC
      T0=T+(GAMA-1.)/(2.*GAMA*R)*Q**2
      P0=P*(T0/T)**(GAMA/(GAMA-1.))
100 RETURN
      END

```

\$IBFTC CEMDAT DECK

BLOCK DATA

```
COMMON/GASFO/GASNAM(10,5,4),GNUM(10,5,4),NML(10,4),
1FZG(10,4),FXG(10,4),ENTHG(10,4),RTEMPG(10,4)
COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
DATA IG1/3/,IG2/4/,IG3/1/,IG4/1/
DATA(GASNAM(1,1,1),I=1,5)/2HS ,2HF ,2H ,2H ,2H /
DATA(GNUM(1,1,1),I=1,5)/1.0,6.0,0.0,0.0,0.0,0.0/
DATA NML(1,1)/1HM/,FZG(1,1)/1HG/,FXG(1,1)/1HF/
DATA(GASNAM(2,1,1),I=1,5)/2HC ,2HF ,2H ,2H ,2H /
DATA (GNUM(2,1,1),I=1,5)/1.0, 4.0,0.0,0.0 ,0.0, 0.0,0.0/
DATA NML(2,1)/1HM/,FZG(2,1)/1HG/,FXG(2,1)/1HF/
DATA(GASNAM(3,1,1),I=1,5)/2HC ,2HH ,2HF ,2H ,2H /
DATA (GNUM(3,1,1),I=1,5)/1.0, 1.0, 3.0,0.0,0.0,0.0/
DATA NML(3,1)/1HM/,FZG(3,1)/1HG/,FXG(3,1)/1HF/
DATA (GASNAM(1,1,2),I=1,5)/2HN ,2H ,2H ,2H ,2H /
DATA (GNUM(1,1,2),I=1,5)/2.0,0.0,0.0,0.0,0.0,0.0/
DATA NML(1,2)/1HM/,FZG(1,2)/1HG/,FXG(1,2)/1HF/
DATA (GASNAM(2,1,2),I=1,5)/2HAR,2H ,2H ,2H ,2H /
DATA (GNUM(2,1,2),I=1,5)/1.0,0.0,0.0,0.0,0.0,0.0/
DATA NML(2,2)/1HM/,FZG(2,2)/1HG/,FXG(2,2)/1HF/
DATA (GASNAM(3,1,2),I=1,5)/2HH ,2H ,2H ,2H ,2H /
DATA (GNUM(3,1,2),I=1,5)/2.0,0.0,0.0,0.0,0.0,0.0/
DATA NML(3,2)/1HM/,FZG(3,2)/1HG/,FXG(3,2)/1HF/
DATA (GASNAM(4,1,2),I=1,5)/2HN ,2HO ,2H ,2H ,2H /
DATA (GNUM(4,1,2),I=1,5)/2.0, 1.0,0.0,0.0,0.0,0.0/
DATA NML(4,2)/1HM/,FZG(4,2)/1HG/,FXG(4,2)/1HF/
DATA (GASNAM(1,1,3),I=1,5)/2HC ,2HO ,2H ,2H ,2H /
DATA (GNUM(1,1,3),I=1,5)/1.0, 2.0, 0.0, 0.0, 0.0/
DATA NML(1,3)/1HM/,FZG(1,3)/1HG/,FXG(1,3)/1HF/
DATA (GASNAM(2,1,3),I=1,5)/2HC ,2HCL, 2HF ,2H ,2H /
DATA (GNUM(2,1,3),I=1,5)/1.0, 1.0, 3.0,0.0,0.0,0.0/
DATA NML(2,3)/1HM/,FZG(2,3)/1HG/,FXG(2,3)/1HF/
END
```

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LMSC/HREC D162424

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$IBFTC ITSUB1 DECK
SUBROUTINE ITSUB (FOFY,Y,SAVE,CONV,NTIMES)
C   REVISED MARCH 5, 1969
C   THIS SUBROUTINE PROVIDES ITERATION CONTROL FOR ANY FUNCTION      0010
C   OF ONE VARIABLE                                                    *20
C   (FOFX)-FUNCTION WHICH IS DRIVEN TO ZERO                            0030
C   (X)-VARIABLE WHICH IS ITERATIVELY SOLVED FOR                       0040
C   (SAVE)-PROGRAM CONTROL                                             050
C   SAVE(1)=ITIME                                                       060
C   SAVE(2)=X INCREMENT                                                0070
C   SAVE(3)=COUNTER DENOTING NTH ITERATION                             0080
C   SAVE(4-7)=STORAGE LOCATIONS FOR X AND FOFX                         0090
C   SAVE( 9-12) = STORAGE LOCATIONS FOR SUCCESSIVE X VALUES
C   SAVE(13-14) = STORAGE LOCATIONS FOR MX AND NXX
C   SAVE(15) = ITERATION TIME SUBTOTAL
C   SAVE(16) = FOFY
C   (CONV)-CONVERGENCE CRITERIA                                       0100
C   (NTIMES)-MAX NUMBER OF ITERATIONS                                  0110
DIMENSION SAVE(16)
MX = SAVE(13)
NXX = SAVE(14)
N1=SAVE(3) +.1                                                         0140
N2=SAVE(15)+1.0
SAVE(16) = FOFY
IF(N2.NE.1) GO TO 5
NXX=0
MX = 8
5 CONTINUE
NX=N2/4 - NXX
FOFXCK=SAVE(8)                                                         0150
C   FOFY AND Y ARE DUMMY INPUT ARGUMENTS                               0160
FOFX=FOFY                                                             0170
X=Y                                                                    0180
C   CHECK FOR CONVERGENCE                                             0190
IF(ABS (FOFX)-CONV.LE.0.)GOTO110                                       0200
ITIME=SAVE(1)+.1                                                       0210
C   ITIME CONTROLS THE TYPE CALCULATION TO BE PERFORMED            0220
C   ITIME=1,FIRST TIME THROUGH                                         0230

```


| | | |
|----|-------------------------------------|------|
| C | ITIME=2, POS FIRST TIME THROUGH | 0240 |
| C | ITIME=3, NEG FIRST TIME THROUGH | 0250 |
| C | ITIME=4, SOLUTION IS BRACKETED | 0260 |
| C | ITIME=5, SOLUTION HAS CONVERGED | 0270 |
| C | ITIME=6, SOLUTION WILL NOT CONVERGE | 0280 |
| C | AJUMP=0.0 | |
| | GOTO(10,30,50,70),ITIME | 0290 |
| C | INITIALIZE | 0300 |
| 10 | N1=1 | 0310 |
| | ITIME=2 | 0320 |
| | FOFXCK=FOFX | 0330 |
| | SAVE(8)=FOFXCK | 0340 |
| | IF(FOFX.LT.0.)GOTO50 | 0350 |
| 30 | IF(FOFX.LT.0.)GOTO70 | 0360 |
| | IF(FOFXCK.GE.FOFX)GOTO35 | 0370 |
| | SAVE(2)=-1.*SAVE(2) | 0380 |
| | X=X-2.*SAVE(2) | 0390 |
| | GOTO90 | 0400 |
| 35 | IF(N1.EQ.1) GO TO 40 | |
| C | ACHECK=(SAVE(5)-FOFX)/SAVE(5) | |
| C | IF(ACHECK.LT.0.3) AJUMP=+1.0 | |
| C | IF(ACHECK.LT.0.2) AJUMP=+2.0 | |
| 40 | SAVE(4)=X | |
| | SAVE(5)=FOFX | 0420 |
| | X=X-SAVE(2) | 0430 |
| | GOTO90 | 0440 |
| 50 | ITIME=3 | 0450 |
| | IF(FOFX.GT.0.)GOTO70 | 0460 |
| | IF(FOFXCK.LE.FOFX)GOTO55 | 0470 |
| | SAVE(2)=-1.*SAVE(2) | 0480 |
| | X=X+2.*SAVE(2) | 0490 |
| | GOTO90 | 0500 |
| 55 | IF(N1.EQ.1) GO TO 60 | |
| C | | |
| C | IF(ACHECK.LT.0.3) AJUMP=-1.0 | |
| C | IF(ACHECK.LT.0.2) AJUMP=-2.0 | |
| 60 | SAVE(6)=X | |
| | SAVE(7)=FOFX | 0520 |

| | | |
|-----|--|------|
| | X=X+SAVE(2) | 0530 |
| | GOTO90 | 0540 |
| 70 | ITIME=4 | 0550 |
| | N1=SAVE(3) | 0560 |
| | N2=0 | |
| | IF(FOFX.LT.0.)GOTO75 | 0570 |
| | SAVE(4)=X | 0580 |
| | SAVE(5)=FOFX | 0590 |
| | GOTO80 | 0600 |
| 75 | SAVF(6)=X | 0610 |
| | SAVE(7)=FOFX | 0620 |
| C | PICK NEW GUESS FOR X ACCORDING TO TYPE CALCULATION | 0630 |
| 80 | X=SAVE(4)-SAVE(5)*((SAVE(6)-SAVE(4))/(SAVE(7)-SAVE(5))) | 0640 |
| 90 | IF(N1.GE.NTIMES)GOTO100 | 0650 |
| C | X=X-AJUMP*SAVE(2) | |
| | MX=MX+1 | |
| | SAVE(MX) = X | |
| | IF(NX.EQ.0) GO TO 92 | |
| | MX = 8 | |
| | NXX=NXX+1 | |
| 92 | CONTINUE | |
| C | TEN ITERATION WILL BE ALLOWED BEFORE MAKING THE TEST OF X VALUE | |
| | IF(N1.LT.10) GO TO 95 | |
| | IF((SAVE(12)-SAVE(10)).NE.0..OR.(SAVE(11)-SAVE(9)).NE.0.) GO TO 95 | |
| C | X VALUE HAS BEEN REPEATING, SET ITIME=4 -- SO THAT THE VALUE OF | |
| C | SAVE(2) CAN BE ADJUSTED IN THE CALLING ROUTINE | |
| | ITIME=4 | |
| | N2=0 | |
| 95 | CONTINUE | |
| | N1=N1+1 | *660 |
| | SAVE(3)=N1 | 0670 |
| | GOTO120 | 0680 |
| 100 | ITIME=6 | 0690 |
| | GOTO120 | 0700 |
| 110 | ITIME=5 | 0710 |
| | SAVE(4)=X | 0720 |
| | SAVE(5)=FOFX | 0730 |
| | SAVE(6)=X | 0740 |

| | | |
|-----|-------------------------|------|
| | SAVE(7)=FOFX | 0750 |
| 120 | SAVE(1)=FLOAT(ITIME)+.1 | 0760 |
| | SAVE(13) = MX | |
| | SAVE(14) = NXX | |
| | SAVE(15)=N2 | |
| | Y=X | 0770 |
| | RETURN | 0780 |
| | END | 0790 |

```

$IBFTC PROTO1 DECK
SUBROUTINE PROTO
C   PRODUCES PROTOTYPE PLUME
COMMON/GASES/TAB(3,12,13),NMIX
COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
COMMON/PLUMF1/PRPR(10,4),REYPLM
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
COMMON/PNT/KPT(4)
COMMON/EXCON/PEX,EMU
DIMENSION H2O(10)
COMMON/MOLFRC/ZFRAC(40),KFR
COMMON /PROSAT/XSAT
INTEGER PNAME
COMMON/PROTG/PNAME(4,5),AOF(4),WTFRAC(2),PNUM(4,5),HENTH(4),
1HTEMP(4),PHAZ(4)
COMMON/SUNUP/SUN(3,40,2)
COMMON/PROTN/RADP,AETP,ANGP,PREP
COMMON/TAPE/IPROT
DATA LLK/1H /
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)      160
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EGRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)    170
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)          180
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)  190
4  ,RHOP,RMW(15),TLN
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2,TOTN(13)
DATA(H2O(1),I=1,7)/-.111333E+03,-.816633E+02,+.273088E+02,+.110650E
$E+01,-.560044E+00,-.191904E-01,+.546921E-02/
DATAWATER,CARBO2/6HH2O  ,6HCO2  /
DIMENSION CO2(10),ARG(10),CON(10)
DATA(CO2(1),I=1,4)/-0.11763432E+03,-0.15185070E+02,+0.15828812E+0
$2,-0.16524522E+01/
C   LOAD GASES INTO CEC ARRAY
DO 20 I=1,5
NAME(1,I)=PNAME(I,I)
20 ANUM(1,I)=PNUM(I,I)

```

```

    PECWT(1)=WTFRAC(1)
    ENTH(1)=HENTH(1)
    RTEMP(1)=HTEMP(1)
    FOX(1)=AOF(1)
    FAZ(1)=PHAZ(1)
    DO 30 I=1,5
    NAME(2,I)=PNAME(2,I)
30  ANUM(2,I)=PNUM(2,I)
    PECWT(2)=WTFRAC(2)
    ENTH(2)=HENTH(2)
    RTEMP(2)=HTEMP(2)
    FOX(2)=AOF(2)
    FAZ(2)=PHAZ(2)
    NAME(3,1)=LLK
    P=PREP
C    IPROT CONTROL WHICH PRODUCTS TAPE WILL BE READ IN CEC
    IPROT=1
    CALL CEC(1,KASE)
    WRITE(6,52)
52  FORMAT(15X,8HH FT2/S2,5X,4HA/A*,7X,5HGAMMA,6X,5HM NO.,10X,5HP PSF,
    16X,7HT DEG R,5X,6HMOL WT)
    NPT=KPT(1)
    WRITE(6,53)(( TAB(1,I,J),I=1,7),J=1,NPT)
53  FORMAT(13X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,2X,E10.3,
    $2X,E10.3)
C    COMPUTE REYNOLDS NO.
    RADTHT=RADP
    AEOAT=AETP
    ANGLP=ANGP
    AT = 3.174*RADP**2
    DEP = 2.*RADTHT*SQRT(AEOAT)
    CALL REYN(1,REY,IRCON)
    WRITE(6,4242) REY
4242 FORMAT(1H0,20X,37HPROTOTYPE EXIT PLANE REYNOLDS NO. IS E10.3)
C    PRODUCE SOURCE FLOW PLUME
    CALL SOURCE(IDUM,ISCON)
C    RESET PROTOTYPE PLUME POINTS TO THOSE AXIAL POSITIONS INPUT
    CALL RESET

```

```

C      COMPUTE APPROXIMATE REYNOLDS NUMBER FOR PROTOTYPE
      IF(ITYPE.EQ.3) CALL REYN(2,REYPL,IRCON)
      IPROT=0
C      RE-INITIALIZE TAB ARRAY TO ZERO
      DO 40 I=1,13
      DO 40 J=1,12
40     TAB(I,J,I)=0.
      REYNP=REY
      REYPLM=REYPL
C      TMAX=647.0
      TMAX = ALOG(300.)
      WRITE(6,778)KFR
      WRITE(6,779)(ZFRAC(IZ),IZ=1,KFR)
778    FORMAT(17H0ZFRAC ARRAY,KFR=15)
779    FORMAT(5X,8E10.3)
C      SEARCH SUN ARRAY FOR CO2
      IH=0
      DO 10 I=1,10
10     CON(I)=CO2(I)
50     IH=IH+1
      WRITE(6,777)SUN(1,IH,1)
777    FORMAT(10X,10HSUN ARRAY ,A6)
      IF(SUN(1,IH,1).EQ. WATER) GO TO 60
      IF(SUN(1,IH,1).EQ.CARB02) GO TO 60
      IF(IH.EQ.KFR)GO TO 55
      GO TO 50
55     XSAT=1000.
      GO TO 150
60     HMOL=ZFRAC(IH)
      WRITE(6,1881) HMOL
1881   FORMAT(17HOHMOLE IN PROTO =E10.3)
      IF(HMOL.LE.1.E-06) GO TO 55
C      SEARCH PLUME FOR SAT. POINT
      IT=0
70     IT=IT+1
C      CHANGE P AND T TO LOG VALUES BECAUSE VAPOR PRES. CURVE FIT
C      IS FOR LOG COOR.
      PL = ALOG(PROP(5,IT)/(14.7*144.)*HMOL)

```

```

      TL= ALOG(PROP(6,IT)/1.8)
      IF(TL.GE.TMAX) GO TO 70
C     PVAP= H2O(1)+H2O(2)*TL +H2O(3)*TL**2+ H2O(4)*TL**3+H2O(5)*TL**4
C     A+H2O(6)*TL**5+ H2O(7)*TL**6
      PVAP = CON(1)+CON(2)*TL+CON(3)*TL**2 +CON(4)*TL**3
      IF(PL.LE.PVAP) GO TO 80
C     FOR BRACKETED POINT
      DT=TH-TL
      DP1=PLH-FL
      DP2= PVAPH-PVAP
      SLP1=DP1/DT
      SLP2=DP2/DT
      GO TO 90
80    CONTINUE
      IF(IT.EQ.1) GO TO 120
      PLH=PL
      PVAPH=PVAP
      TH=TL
      GO TO 70
90    CONTINUE
      TINSCT = EXP((PVAP-PL + TL*(SLP1-SLP2))/(SLP1-SLP2))
      TLI = ALOG(TINSCT)
      PINSCT = EXP(SLP1*(TLI-TL)+PL)
      PTINS = PINSCT/HMOL
C     COMPUTE AXIAL LOCATION OF CONDENSATION
      SLPX = ALOG(PROP(5,IT)/PROP(5,IT-1))/ALOG(PROP(1,IT)/PROP(1,IT-1))
      ONOS= 1./SLPX
      XINSCT= PROP(1,IT-1)*EXP(ONOS*ALOG(PTINS/PROP(5,IT-1)))
      WRITE(6,100) XINSCT
100   FORMAT(10X,38HPROTOTYPE CONDENSATION OCCURS AT .....E10.3)
      GO TO 130
120   WRITE(6,121)
121   FORMAT(10X,56HSATURATION OCCURS IN OR NEAR NOZZLE, XINSCT SET TO
      *ZERO)
      XINSCT=0.
130   XSAT = XINSCT
150   CONTINUE
      RETURN
      END

```

```

$*
$ORIGIN      B
$IBFTC COMP
  SUBROUTINE COMPAR(ITYP,ICK,IRCON,KASE)
  COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
  COMMON/GASES/TAB(3,12,13),NMIX
  COMMON/SUNUP/SUN(3,40,2)
  COMMON/WRIT/IFLG1
  COMMON/TAPE/IPROT
  COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
  COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DELM,DELMN,
$DELREY
  COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
  COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
  COMMON/PLUMF1/PRPR(10,4),REYPLM
  DIMENSION EP(50),EPS(5)
  ICK=0
  KACE = KASE
  IF(ITYP.GT.1)GO TO 100
  CALL REYN(1,REY,IRCON)
  WRITE(6,5)REY
  5  FORMAT(20X,21HSIMULANT RN AT EXIT =,E10.3)
  IF(REY.LT.REYNP)ICK=2
  GO TO 300
100  CONTINUE
  CALL RESET
  GO TO (120,130,140),ITYPE
120  CONTINUE
C    COMPARE PLUME REGION FOR MOMENTUM FLUX
  EPSUM=0
  DO 50 J=1,3
  G1=GMC(J)
  P1=PC(J)
  EM1=EMC(J)
  G2=PRPR(3,J)
  P2=PRPR(5,J)
  EM2=PRPR(4,J)
C    COMPUTE ERROR

```



```

      EPS(J)=FMOM(G1,P1,FM1)-FMOM(G2,P2,EM2)
      EPSUM=EPSUM+EPS(J)
50  CONTINUE
      EP(KACE)=EPSUM
      WRITE(6,60)EPSUM,KACE
60  FORMAT(2CX,23HSUMMATION OF MOM ERROR=,E10.3,2X,10HFOR CASE ,I5)

C
C   ALSO COMPARE CENTER PT.
      DELM=EPS(2)
      PCM=DELM/FMOM(PRPR(3,2),PRPR(5,2),PRPR(4,2))
      WRITE(6,70)DELM,PCM
70  FORMAT(1H2,5HDELM=,E10.3,5X,4HPCM=,E10.3)
      IF(ABS(PCM).GT..1*ERRMAX)ICK=3
      GO TO 300
130 CONTINUE
C   COMPARE PLUME REGION FOR MACH NO.
      DELMN=EMC(4)-PRPR(4,2)
      PCMN = DELMN/PRPR(4,2)
      WRITE(6,132) DELMN,PCMN
132 FORMAT(20X,17HOMACH NO. ERROR= E10.3,2X,18HPERCENTAGE ERROR= E10.3)
      $)
      IF(ABS(PCMN).GT..1*ERRMAX) ICK=3
      GO TO 300
140 CONTINUE
C   COMPARE PLUME REGION FOR REYNOLDS NJMBER
      CALL REYN(2,REYM,IRCON)
      DELREY=REYPLM-REYM
      PCREY= DELREY/REYNP
      WRITE(6,142) DELREY,PCREY
142 FORMAT(20X, 21HOREYNOLDS NO. ERROR= E10.3,2X,18HPEPCENTAGE ERROR =,
1E10.3)
      IF(ABS(PCREY).GT..1*ERRMAX) ICK=3
300 CONTINUE
      RETURN
      END

```

```
$IBFTC FMOM1 DECK  
FUNCTION FMOM(G,P,EM)  
FMOM=G*P*EM**2  
RETURN  
END
```

```

$IBFTC REYN1
  SUBROUTINE REYN(LTYPE,REY,IRCON)
C   SUBROUTINE REYN COMPUTES REYN. NO. AT EXIT PLANE
C   USING PROPERTIES FROM THE TAB ARRAY
C
  COMMON/GASES/TAB(3,12,13),NMIX
  COMMON/SUNUP/SUN(3,40,2)
  COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
  COMMON/NUMG/IG1,IG2,IG3,IG4,PCMAX,IG
  COMMON/GASCON/GAMA,R,T0,P0,EM,RHO,T,WM ,Q
  COMMON/GEOM/AT,RADTHT,AE0AT,ANGLP,REYNP
  COMMON/EXCON/PEX,EMU
  COMMON/PLUMF1/PRPR(10,4),REYPLM
  COMMON/TAPE/IPROT
  COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
  COMMON/MOLFRC/ZFRAC(40),KFR
  COMMON/WRIT/IFLG1
  COMMON/COUNT/IKLUG
  DIMENSION SAVEA(16)
  DATA (SAVEA(K),K=1,16) /16*0./
  EQUIVALENCE (GAMA,GAMA)
  IRCON=0
C   REYN COMPUTES REYNOLDS NO. AT AT PT. KNOWING THE THERMO
C   PROPERTIES..... EXIT CONDITIONS ARE GENERALLY CALLED
C   FIRST GUESS FOR EXIT PRESSURE
  P=.005*TAB(1,5,1)
  SSQR=AE0AT
  TOL=0.005*SSQR
  SAVEA(1)=1.0
  PINC=-.09*P
  SAVEA(2)=PINC
  PSTAR=TAB(1,5,2)
  CALL TABLE(PSTAR,1)
  RSTAR=RHO
  QSTAR=Q
C   BYPASS EXIT PLANE CALC IF PLUME RN IS DESIRED
  IF(LTYPE.EQ.2)GO TO 200
18 CONTINUE

```

```

      IF(P.GT.0.)GO TO 30
      P=P-.95*PINC
      PINC=.1*PINC
      SAVEA(2)=PINC
30  CONTINUE
      CALL TABLE(P,1)
      ARAT=RSTAR*QSTAR/(RHO*Q)
      FP= SSQR-ARAT
      GO TO 198
          WRITE(6,39)
39  FORMAT(20H0TABLE CHECK--GASCON)
      WRITE(6,40)GAMA,R,T0,P0,EM,RHO,T,WM,Q
40  FORMAT(10X,9E10.3)
      WRITE(6,4000)RHO,Q,GAMA,GAMMA
4000 FORMAT(1H0,4HRHO=E10.3,2HQ=E10.3,5HGAMA=E10.3,6HGAMMA=E10.3)
      WRITE(6,100)SSQR,ARAT,FP,P,SAVEA(2)
100  FORMAT(6H0SSQR=,E10.3,5HARAT=,E10.3,3HFP=,E10.3,5HPRES=,E10.3,
15HPINC=,E10.3)
198  CONTINUE
      CALL ITSUB(FP,P,SAVEA,TOL,199)
      II=SAVEA(1)+.1
      N1=SAVEA(3)+.1
      GO TO (18,18,18,18,22,23),II
23  WRITE(6,600)FP,P
600  FORMAT(36H0ITSUB WILL NOT CONVERGE IN REYN,FP=,E10.3,5X,2HP=,E10.3
1)
      IRCON=1
      RETURN
22  CONTINUE
      PEX = P
      GO TO 300
200  CONTINUE
C    LOAD PLUME PROPERTIES INTO P AND T
      IF(IPROT.EQ.1) GO TO 210
      P=PC(2)
      T=TC(2)
      GO TO 300
210  P=PRPR(5,2)

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      T=PRPR(6,2)
300 CONTINUE
      GO TO 400
      IF(IPROT.EQ.1) GO TO 400
      TR=T
C     THE FIRST DIGIT IN TAB AND SUN INDICATES IF GAS IS MIXTURE
C     OR COMPONENT
C     3RD DIGIT OF SUN INDICATES PART OF GAS NAME
C     FIRST LOAD THE NAME INTO TEMP
      K=NMIX+8
      DO 5 KM=1,NMIX
        TEMP(1,KM+7)=SUN( 1,KM,1)
      5 TEMP(2,KM+7)=SUN(1,KM,2)
C     LOAD MOLE FRACTION INTO TEMP
C     IF PROTOTYPE CALC.. USE MOLE FRAC. FROM ZFRAC
      IF(IPROT.EQ.1)GO TO 70
      DO 10 KM=9,K
10    TEMP(3,KM-1)=TAB(1 ,KM,1)
      GO TO 80
70    CONTINUE
      DO 75 KL=1,KFR
75    TEMP(3,KL+7)=ZFRAC(KL)
80    CONTINUE
      IWRT=1
      WRITE(6,16)
16    FORMAT(51HORE WRITING GAS NAME AND MOLE FRACTION USED IN REYN)
      DO 17 N=1,NMIX
17    WRITE(6,28) TEMP(1,N+7),TEMP(2,N+7),TEMP(3,N+7)
28    FORMAT(1H0,5X,2A6,E10,3)
15    CONTINUE
      CALL TRANS(TR,1,EMU)
C     COMPUTATION OF REYNOLDS NO.
      REX =RADTHT*SQRT(AEOAT)
      EMU=EMU*.0671983
      REY= RHO*Q*2.0*REX/EMU
      GO TO 500
400 ROUSTR=RSTAR*QSTAR
      VIS = .1335E-4*(T/1.8)**.95
      EL= RADTHT*SQRT(AEOAT)
      REY=ROUSTR*2.*EL/VIS
500 CONTINUE
      RETURN
      END

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$ORIGIN      C
$IBFTC CONDNS
SUBROUTINE CONDEN(ICON,ISWTC,HACP,TONEW)
COMMON/GASES/TAB(3,12,13),NMIX
C COEFFICIENTS FOR VAPOR PRESSURE CURVES ARE COMPUTED FOR LOG
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/PROSAT/XSAT
COMMON/SUNUP/SUN(3,40,2)
COMMON/MOLFRC/ZFRAC(40),KFR
COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
COMMON/MGEOM/ATM,RADTHM,AEOATM,ANGLPM
DATA CARB02/6HCO2 /
C COMPARE PROPERTY ALONG EXPANSION--PROP--WITH VAPOR PRESSURE
C CURVE
C TYPE FIT, THUS THE CONVERSION OF THE PLUME DATA.
C
DIMENSION CO2(10),ARG(10),CON(10)
DATA(CO2(I),I=1,4)/-0.11763432E+03,-0.15185070E+02,+0.15828812E+0
$2,-0.16524522E+01/
C TEST GAS TYPE
IF(ICON.EQ.2)GO TO 20
DO 10 I=1,10
10 CON(I)=CO2(I)
TMAX=ALOG(300.)
GO TO 40
20 DO 30 I=1,10
30 CON(I)=ARG(I)
TMAX=ALOG(300.)
40 CONTINUE
IH =0
150 IH=IH+1
WRITE(6,777)SUN(1,IH,1)
777 FORMAT(10X,10HSUN ARRAY ,A6)
IF(SUN(1,IH,1).EQ.CARB02) GO TO160
GO TO150
160 XCON=ZFRAC(IH)
WRITE(6,500)XCON
500 FORMAT(20X,5HXCON=E10.3)

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      I=0
50  I=I+1
      P1= ALOG (PROP(5,I)*XCON/(14.7*144.))
      T1=ALOG (PROP(6,I)/1.8)
      IF(T1.GE.TMAX)GO TO 50
      ISWTC=0
      P2=CON(1)+CON(2)*T1+CON(3)*T1**2+CON(4)*T1**3
C    TEST IF LINES CROSS
      IF(P1.LE.P2)GO TO 60
C    NOW HAVE INTERSECTION BRACKETED
      DT=TH-T1
      DP1=P1H-P1
      DP2=P2H-P2
      SLP1=DP1/DT
      SLP2=DP2/DT
      GO TO 80
60  P1H=P1
      P2H=P2
      TH=T1
      GO TO 50
80  TINRST=(P2-P1+T1*(SLP1-SLP2))/(SLP1-SLP2)
      PINRST= SLP1*(TINRST-T1)+P1
      WRITE(6,501)P1,T1,P2,DT,SLP1,SLP2,TINRST,PINRST
501 FORMAT(10X,8E10.3)
C
C    OBTAIN MOLE FRACTION OF CONDENSANT
C    NOW INTERPOLATE FOR AXIAL POSITION OF CONDENSATION
C    FIRST CALC. ACTUAL PRESSURE AND TEMP
      TI=EXP(TINRST )
      PIT = EXP(PINRST)
      PI = PIT*14.7*144./XCON
      WRITE(6,90)
90  FORMAT(20X,31HOCONDENSATION PROPERTIES FOLLOW)
      WRITE(6,91)TI,PI
91  FORMAT(1H0,19X,3HT2=,E10.3,2X,3HPI=,E10.3)
      X1H=PROP(1,I-1)
      SLPX=ALOG(PROP(5,I)/PROP(5,I-1))/ALOG(PROP(1,I)/PROP(1,I-1))
      ONOM=1./SLPX

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      XI=XIH*EXP(ONOM*ALOG(PI/PROP(5,I-1)))
      WRITE(6,100)XI
100  FORMAT(1H0,14X,28HSIMULANT CONDENSATION PT. IS,E10.3)
C    COMPUTE PERCENT DIFFERENCE
      DX=XSAT-XI
      DEPM = 2.*RADTHM*SQRT(AEOAT)
      DIFF = 20.*DEPM
C    DETERMINE IF ERROR ACCEPTABLE
      IF(XI.GT.XC13.AND.XSAT.GT.XC13)GO TO 200
      IF(DX.LE.DIFF) GO TO 200
      ISWTCH=1
C    IF NOT COMPUTE A DESIRED CHANGE IN TO TO ADJUST THE PT.
      GOGM1=(PROP(3,I)-1.)/PROP(3,I)
C
C    KNOWING DESIRED SATURATION POSITION A NEW PRESSURE IS COMPUTED
      PNEW= PI*EXP(SLPX*ALOG(XSAT/XI))
      DELP= PNEW-PI
      IACP=1
      TONEW= (DELP/TAB(1,5,1))*GOGM1*TAB(1,6,1)*DELP**(1./SLP1)
C    IS TONEW ACCEPTABLE
      IF(TONEW.LT.2000.)IACP=0
      WRITE(6,105)TONEW
105  FORMAT(1H0,20X,18HNEW TO COMPUTED IS,E10.3)
200  RETURN
      END

```



```

$IBFTC REST1 DECK
SUBROUTINE RESET
COMMON/TAPE/IPROT
COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
COMMON/PLUMF1/PRPR(10,4),REYPLM
COMMON/PLUMF2/PROP(10,200),IPT
COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
C RESETS SIMULANT PLUMF PTS. TO THOSE STATIONS
C COMPUTED FOR PROTOTYPE CASE
IF(IPROT.EQ.1) GO TO 40
I=0
J=0
5 J=J+1
10 I=I+1
IF(PRPR(1,J).GT.PROP(1,I))GO TO 10
XQ=PRPR(1,J)
XC(J)=XQ
SLP1=ALOG(PROP(5,I)/PROP(5,I-1))/ALOG(PROP(1,I)/PROP(1,I-1))
PC(J)= PROP(5,I-1)*EXP(SLP1*ALOG(XQ/PROP(1,I-1)))
C
SLP2=(PROP(4,I)-PROP(4,I-1))/(PROP(1,I)-PROP(1,I-1))
EMC(J)= SLP2*(XQ-PROP(1,I-1))+PROP(4,I-1)
C
SLP3=(PRPR(3,I)-PRPR(3,I-1))/(PROP(1,I)-PROP(1,I-1))
GMC(J)=SLP3*(XQ-PROP(3,I-1))+PROP(3,I-1)
XSIP=ALOG(PROP(5,I-1)/PROP(5,I))/ALOG(PROP(6,I-1)/PROP(6,I))
ONOX=1.0/XSIP
TC(J)= PROP(6,I-1)*(PC(J)/PROP(5,I-1))*ONOX
RGC=1545./PROP(7,I-1)*32.174
A=GMC(J)*RGC*TC(J)
QC(J)= EMC(J)*SQRT(A)
EMWC(J)=PROP(7,I-1)
NPTS=3
IF(J.EQ.NPTS)GO TO 20
GO TO 5
20 CONTINUE
WRITE(6,25)
25 FORMAT(1H0,10X,35H SIMULANT PLUME PROPERTIES AT X-CUTS)

```

```

WRITE(6,27)
27 FORMAT(1H0,20X,1HX,10X,2HPC,10X,1HM,10X,1HG,10X,1HT,10X,2HMW,
110X,1HQ)
WRITE(6,26)(XC(J),PC(J),EMC(J),GMC(J),TC(J),EMWC(J),QC(J),J=1,3)
26 FORMAT(25X,7E10.3)
GO TO 100
40 CONTINUE
C THE FOLLOWING SECTION PICKS OUT PROTOTYPE PTS IN REGION
XC(1)=XC11
XC(2)=XC12
XC(3)=XC13
I=0
J=0
45 I=I+1
50 J=J+1
IF(XC(I).GT.PROP(1,J))GO TO 50
FAC1=ALOG(PROP(5,J)/PROP(5,J-1))/ALOG(PROP(1,J)/PROP(1,J-1))
PRPR(5,I)=PROP(5,J)*EXP(FAC1*ALOG(XC(I)/PROP(1,J-1)))
FAC2=(PROP(4,J)-PROP(4,J-1))/(PROP(1,J)-PROP(1,J-1))
PRPR(4,I)=PROP(4,J-1)+FAC2*(XC(I)-PROP(1,J-1))
FAC3=(PROP(3,J)-PROP(3,J-1))/(PROP(1,J)-PROP(1,J-1))
PRPR(3,I)=PROP(3,J-1)+FAC3*(XC(I)-PROP(1,J-1))
ONOX=1./((ALOG(PROP(5,J-1)/PROP(5,J))/ALOG(PROP(6,J-1)/PROP(6,J)))
1)
PRPR(6,I)=PROP(6,J-1)*(PRPR(5,I)/PROP(5,J-1))*ONOX
PRPR(7,I)=PROP(7,J-1)
PRPR(1,I)=XC(I)
IF(I.EQ.3)GO TO 70
GO TO 45
70 CONTINUE
WRITE(6,75)
75 FORMAT(20X,33HPROTOTYPE PLUME POINTS FOR REGION)
WRITE(6,80)
80 FORMAT(15X,1HX,10X,5HM NO.,10X,5HGAMMA,10X,1HP,10X,1HT,10X,2HMW)
DO 90 IP=1,3
WRITE(6,85)PRPR(1,IP),PRPR(4,IP),PRPR(3,IP),PRPR(5,IP),PRPR(6,IP),
1PRPR(7,IP)
85 FORMAT(10X,6(E10.3,4X))
90 CONTINUE
100 CONTINUE
RETURN
END

```

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\$*
\$ORIGIN C

LMSC/HR/EC D162424

```

$IBFTC TRAN    DECK
      SUBROUTINE TRANS(TE,JDUM,VIS)
C
C**  PROGRAM WHICH CALCULATES TABLE OF VISCOSITY, CP AND THERMAL
C     CONDUCTIVITY FROM THE NASA-LEWIS EQUILIBRIUM CHEMISTRY DATA
C
C     TO LESSEN THE NO. OF CHANGES THAT MUST BE MADE, THE THERMODYNAMIC
C     DATA FOR THE TRANSPORT PROPERTIES WILL BE READ FROM TAPE 12, THE
C     OLD NASA/LEWIS DATA TAPE.
C     THE THERMODYNAMIC DATA FOR THE CEC PORTION WILL BE READ FROM TAPE
C     4, THE NEW DATA TAPE GENERATED BY MCDERMIT.
C     TO MAKE THESE COMPATABLE THE CEC IS MODIFIED TO READ THE GAS NAME
C     UNDER A 2A6 FORMAT.
      DIMENSION ZETA(4),BETA(4),BETEND(4)
      COMMON/SPDATA/AA(90,5),XMF(90),XMW(90),SIGMA(90),OMEGA(90),TR,N
      COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
      COMMON/THRMTR/A(90,15)
      COMMON/MO/NUM(90)
      COMMON/GASES/TAB(3,12,13),NMIX
      DATA (BETEND(I),I=1,4)/4*6HEND
      COMMON/WRIT/IFLG1
      COMMON/COUNT/IKLUG
      IDATA=NMIX+7
      TR=TE
      REWIND 13
      IV=3
C**  LOOP WHICH CALCULATES FLOW PROPERTIES
      DO 54 J=3,IV
1030  FORMAT(1H , (7E18.7))
      IF(TR.LT. 1.0) GO TO 9000
      KT = 0
      DO 55 K=8,IDATA
      IF(TEMP(J,K).LT..000005)GO TO 55
      IF(TEMP(J,K).GT.1.0   ) GO TO 55
      KT = KT + 1
C
C**  GAS SPECIE NAMES
C

```

```

        SPNAM1(KT) = TEMP(1,K)
        SPNAM2(KT) = TEMP(2,K)
55  CONTINUE
    IF(KT.EQ.0) GO TO 999
C
C**  LOCAL TEMPERATURE
    IERR = 0
    CALL GTLUP(J,IERR,IFIRST)
    IF(IERR.LQ.1) GO TO 99
C
C**  CALCULATE VISCOSITY,CP,CONDUCTIVITY
C
    CALL PROPTY( VIS,COND,CP)
    TEMP(J,IDATA+1) = VIS
    TEMP(J,IDATA+2) = COND
    TEMP(J,IDATA+3) = CP
    GO TO 54
999  WRITE(6,1000)I,J
1000 FORMAT(1H0,33HNO SPECIE DATA FOR ENTROPY CUT = ,I2, 17H VELOCITY
    ICUT = ,I2)
    TEMP(J,IDATA+1) = 0.
    TEMP(J,IDATA+2) = 0.
    TEMP(J,IDATA+3) = 0.
    GO TO 54
9000 WRITE(6,9001)
9001 FORMAT(1H , 20HNegative TEMPERATURE )
    TEMP(J,IDATA+1) = 0.
    TEMP(J,IDATA+2) = 0.
    TEMP(J,IDATA+3) = 0.
54  CONTINUE
99  CONTINUE
C
    RETURN
    END

```

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$ORIGIN          D
$IBFTC PROP     DECK
C
  SUBROUTINE PROPTY(      VISCOS,COND, CP)
C** THIS SUBROUTINE CALCULATES THE GAS VISCOSITY, THERMAL CONDUCTIVITY
C AND CP AS A FUNCTION OF TEMPERATURE
  DIMENSION TABLJP(131)
  DIMENSION CPR(90), XP(4,90), F(4),XA(90),D(90,90)
  COMMON/WRIT/IFLG1
  COMMON/SPDATA/AA(90,5),XMF(90),XMW(90),SIGMA(90),OMEGA(90),TR,N
C** THIS TABLE IS THE REDUCED COLLISION INTEGRAL FROM HIRSHFELDER
  COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
C 1 THE HIRSHFELDER SYMBOL EQUALS OMEGA***2.2
  DATA TABLJP /65., .3 , .4 , .5 , .6 , .7 , .8 , 01150
* .9 , 1. , 1.1 , 1.2 , 1.3 , 1.4 , 1.5 , 1.6 , 01160
* 1.7 , 1.8 , 1.9 , 2.0 , 2.1 , 2.2 , 2.3 , 2.4 , 01170
* 2.5 , 2.6 , 2.7 , 2.8 , 2.9 , 3.0 , 3.1 , 3.2 , 01180
* 3.3 , 3.4 , 3.5 , 3.6 , 3.7 , 3.8 , 3.9 , 4.0 , 01190
* 4.1 , 4.2 , 4.3 , 4.4 , 4.5 , 4.6 , 4.7 , 4.8 , 01200
* 4.9 , 5. , 6. , 7. , 8. , 9. , 10. , 20. , 01210
* 30. , 40. , 50. , 60. , 70. , 80. , 90. , 100. , 01220
* 200. , 300. , 400. , 01230
$ 2.785 , 2.492 , 2.257 , 2.065 , 1.908 , 1.780 , 01240
$ 1.675 , 1.587 , 1.514 , 1.452 , 1.399 , 1.353 , 1.314 , 1.279 , 01250
$ 1.248 , 1.221 , 1.197 , 1.175 , 1.156 , 1.138 , 1.122 , 1.107 , 01260
$ 1.093 , 1.081 , 1.069 , 1.058 , 1.048 , 1.039 , 1.030 , 1.022 , 01270
$ 1.014 , 1.007 , .9999, .9932, .9870, .9811, .9755, .9700, 01280
$ .9649, .9600, .9553, .9507, .9464, .9422, .9382, .9343, 01290
$ .9305, .9269, .8963, .8727, .8538, .8379, .8242, .7432, 01300
$ .7005, .6718, .6504, .6335, .6194, .6076, .5973, .5882, 01310
$ .5320, .5016, .4811/ 01320
C
C THE AA ARRAY IS DEFINED AS THE FOLLOWING
C ** THIS DATA TAKEN FROM NASA LEWIS THERMOCHEMISTRY DATA DECK **
C
C 1 THE FIRST FIVE NUMBERS OF EACH TWO CARD SET
C 2 ARE POLYNOMIAL COEFFICIENTS OF A CURVE FIT
C 3 OF CP/R FOR A TEMPERATURE RANGE DEPENDING ON TK

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C      XMF=MASS FRACTION
C      XMW=MOLECULAR WEIGHT
C      CPR=CPAR
C      RU=UNIVERSAL GAS CONSTANT
C      VISCOS=VISCOSITY
C      COND=THERMAL CONDUCTIVITY
C      CP=SPECIFIC HEAT AT CONSTANT PRESSURE
      TK = TR/ 1.8
      RU = 1.98726
      DO 840 I = 1, N
      XP(4, I) = XMW(I)
      CPR(I) = AA(I,1)
      DO 830 J = 2, 5
      AT = AA(I,J)
      DO 820 JJ= 2,J
820    AT = AT * TK
830    CPR(I) = CPR(I) + AT
      XP(3,I) = CPR(I)
840    CONTINUE
      DO 850 I = 1, N
      TRED = TK / OMEGA(I)
      CALL ONEVAR( TRED, 2, TABLJP, 1, 131, OMERED)
      IF(IFLG1.EQ.0)GO TO 191
      WRITE(6,1032)TRED,OMERED,I
1032  FORMAT(1H0, 6HTRED =,E15.7,5X, 8HOMERED =, E15.7, 5X, 3H I=,I3)
      191 CONTINUE
      XP(1, I)=266.93 *10.**(-7)*SQRT(XMW(I)*TK )/(SIGMA(I)**2*OMERED)
850    XP(2, I) =(RU/XMW(I))*(3.75 +1.32*(CPR(I)- 2.5))*XP(1, I)
      IF(IFLG1.EQ.0)GO TO 192
      WRITE(6,1035)
1035  FORMAT(1H , 35HRESULTS OF TRANSPORT PROPERTY CALCS,/, 6HSPECIE,7X
      1, 6HVISCOS,8X, 4HCOND,10X, 2HCP, 12X, 7HMOL, WT,7X, 9HMOL FRACT,
      2 5X, 5HOMEGA, 9X, 5HSIGMA, 9X,11HTEMP(DEG K),/)
      192 CONTINUE
      DO 600 I=1,N
      IF(IFLG1.EQ.0)GO TO 193
600    WRITE(6,1040) SPNAM1(I),SPNAM2(I),(XP(K,I),K=1,4),XMF(I),OMEGA(I),
      1 SIGMA(I),TK

```

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```

1040 FORMAT(1H0, 2A6,1X,(8(E12.5,2X)))
193 CONTINUE
900 CONTINUE
DO 500 K = 1,4
C
C FOR K = 1 VISCOSITY OF MIXTURE CALCULATED
C K = 2 CONDUCTIVITY OF MIXTURE CALCULATED
C K = 3 CP OF MIXTURE CALCULATED
C K = 4 MOLE WEIGHT OF MIXTURE CALCULATED
C
VISCOS = 0.
COND = 0.
CP = 0.
OLWT = 0.
F(K) = 0.
DO 400 I=1,N
XA(I) = 0.0
IF (K.EQ.4) GO TO 320
DO 300 J=1,N
IF (J .EQ. 1) GO TO 300
D(I,J) = .376*(1. + SQRT(XP(K,I) / XP(K,J)) * (XMW(J)/XMW(I))
1      ** .25)**2*SQRT(XMW(J)/(XMW(I)+XMW(J)))
XA(I) = XA(I) + XMF(J) * D(I,J)
300 CONTINUE
IF(XMF(I).LT..000001) GO TO 400
310 F(K) = F(K) + (XMF(I) * XP(K,I)) / (XMF(I) + XA(I))
GO TO 400
320 F(K) = F(K) + XP(K,I)*XMF(I)
400 CONTINUE
500 CONTINUE
C UNITS-POISES
VISCOS=F(1)
C UNITS-ENGLISH
COND = F(2)
C UNITS-BTU/LBM/DEG-R
CP = F(3) * RU / F(4)
OLWT = F(4)
RETURN
END

```

```

01730
01740
01750
01760
01770
01780
01790
01800
01810
01820
01830
01840
01850
01860
01870
01880
01890
01900
01910
01930
01940
01950
01960
01970
02000
02010
02020
02030

```

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```

$IBFTC ONEV    DECK
      SUBROUTINE ONEVAR (ARGUMT,NXDIR, TABLE, NOTAB, NX, OUTPUT)          02050
C                                                    2060
C ONEVAR IS AN INTERPOLATION ROUTINE - ONE FUNCTION OF ONE          02070
C ARGUMENTS OF THE SUBROUTINE ARE AS FOLLOWS                          02080
C   ARGUMT   = INPUT INTERPOLATION ARGUMENT (X)                       02090
C   NXDIR    = TYPE OF INTERP. 1 FOR LINEAR, 2 FOR QUAD.              02100
C   TABLE   = SET OF X VALUES FOLLOWED BY THE Y VALUES            02110
C   OUTPUT   = INTERPOLATED VALUE OF Y = F(X)                        02120
C   NER      = ERROR CODE                                             02130
C       1 = OK, INTERPOLATION SUCCESSFUL.                             02140
C       2 = OFF CHART LOW END. MIN. VAL. SUBSTITUTED                 02150
C       3 = OFF CHART HIGH END. MAX. VAL. SUBSTITUTED               02160
C       4 = NO. OF X ENTRIES IS NOT 2 TO 15 (IF NXDIR               02170
C           IS 1). OR, IT IS NOT 3 TO 15 (IF NXDIR                    02180
C           IS 2).                                                    02190
C       5 = X ENTRIES NOT IN ASCENDING ORDER.                       02200
C
C   TABLE IS LOADED AS      LOC.      VALUE                          02210
C   TABLE(1)                NO. OF X VALUES                       02220
C   TABLE(2)                X(1)                                    02230
C
C                               ETC                                    02240
C   TABLE(N+1)              X(N)                                    02250
C   TABLE(N+2)              Y(1)  WHERE  Y = F(X)                  02260
C
C                               ETC                                    02270
C   TABLE(N+1+N)            Y(N)                                    02280
C
C                               ETC                                    02290
C   TABLE(N+1+N)            Y(N)                                    02300
C
C   DIMENSION TABLE(NX)                                           02310
C   NOENTR = INT(TABLE(1))                                           02320
C   N = NOENTR                                                         02330
C   NER = 1                                                             02340
C   IF (NXDIR-1) 1,1,2                                               02350
1 IF (NOENTR-2) 4,3,3                                               02360
2 IF (NOENTR-3) 4,3,3                                               02370
3 IF (NXDIR + 1 - NOENTR ) 5, 9, 4                                  02380
4 NER = 4                                                             02390

```


| | |
|--|-------|
| GO TO 701 | 02420 |
| 5 IF (ARGUMT-TABLE(2)) 6,7,10 | 02430 |
| 6 NER = 2 | 02440 |
| GO TO (23, 32), NXDIR | 02450 |
| 7 NER = 1 | 02460 |
| 8 IOUT = 2 | 02470 |
| GO TO 700 | 02480 |
| 9 GO TO (23, 32), NXDIR | 02490 |
| 10 IF (TABLE(NOENTR+1)-ARGUMT) 11,13,16 | 02500 |
| 11 NER = 3 | 02510 |
| I = N - 1 | 02520 |
| GO TO (25, 31),NXDIR | 02530 |
| 13 NER = 1 | 02540 |
| 14 IOUT = NOENTR+1 | 02550 |
| 15 GO TO 700 | 02560 |
| C AT THIS STAGE OF THE GAME, ERROR CONDITIONS 2,3,4 HAVE | 02570 |
| C BEEN TESTED FOR AND HAVE BEEN PASSED. | 02580 |
| 16 DO 100 JK=1, NOENTR | 02590 |
| I = JK | 02600 |
| IF (I-1) 20,20,17 | 02610 |
| 17 IF (TABLE(I+1)-TABLE(I)) 18,18,20 | 02620 |
| 18 NER = 5 | 02630 |
| GO TO 701 | 02640 |
| 20 IF (TABLE(I+1)- ARGUMT) 99,21,24 | 02650 |
| 99 IF (I .GE. N) GO TO 11 | 02660 |
| 100 CONTINUE | 02670 |
| 21 NER = 1 | 02680 |
| IOUT = I+1 | 02690 |
| GO TO 700 | 02700 |
| 23 I = 2 | 02710 |
| 24 IF (NXDIR-1) 25,25,29 | 02720 |
| 25 ION = I + N | 02730 |
| OUTPUT = TABLE(ION)+ (ARGUMT - TABLE(I)) * (TABLE | 02740 |
| I(ION+1)- TABLE(ION))/(TABLE(I+1)-TABLE(I)) | 02750 |
| GO TO 701 | 02760 |
| 29 IF (NOENTR - I) 31, 30, 33 | 02770 |
| 30 I = I-1 | 02780 |
| GO TO 31 | 02790 |

| | | |
|----------|--|-------|
| 32 | I = 2 | 02800 |
| 33 | IF (I .EQ. 1) I = 2 | 02810 |
| 31 | ION = I + N | 02820 |
| | CA=(TABLE(ION)*(ARGUMT-TABLE(I+1))*(ARGUMT-TABLE(I+2))) | |
| | CB=(TABLE(I)-TABLE(I+1)) | |
| | CD=(TABLE(I)-TABLE(I+2)) | |
| | CE=((TABLE(ION+1)*(ARGUMT - TABLE(I)))*(ARGUMT-TABLE(I+2))) | |
| | CF=((TABLE(I+1)-TABLE(I))*(TABLE(I+1)-TABLE(I+2))) | |
| | OUTPUT= (CA)/(CB * CD)+(CE)/(CF) + (TABLE(ION+2)*(ARGUMT - | |
| | TABLE(I)) * (ARGUMT - TABLE(I+1)))/((TABLE(I+2)- | 02880 |
| | TABLE(I)) *(TABLE(I+2) - TABLE(I+1))) | 02890 |
| | GO TO 701 | 02900 |
| 700 | IOUT = IOUT + N | 02910 |
| | OUTPUT = TABLE(IOUT) | 02920 |
| 701 | IF (NER - 2) 800, 707, 706 | 02930 |
| 706 | IF (NER - 4) 707, 711, 714 | 02940 |
| 707 | GO TO 800 | 02950 |
| 711 | WRITE(6,712) NOTAB | 02960 |
| 712 | FORMAT(1H ,28HTOO FEW ENTRIES IN TABLE NO., I4) | 02970 |
| | GO TO 800 | 02980 |
| 714 | WRITE (6, 715) NOTAB | 02990 |
| 715 | FORMAT(1H ,57HENTRIES ARE NOT IN MONOTOMIC ASCENDING ORDER IN TABL | 03000 |
| | 1E NO.,I4) | 03010 |
| 800 | RETURN | 03020 |
| | END | 03030 |
| \$ORIGIN | D | |

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LMSC/HREC D162424

```

$IBFTC GTLU    DECK
      SUBROUTINE GTLUP(J,IERR,IFIRST)
C
C**  THIS SUBROUTINE DOES A TAPE LOOK UP TO OBTAIN DATA REQUIRED FOR
C    COMPUTATION CP,MU AND K
      DIMENSION DDD(90,5)
      COMMON/WRIT/IFLG1
      COMMON/DRAY/B(5,100),KD
      DIMENSION TITLT(4),D(5),DD(15,4),TITLE(4),TEND(4)
      COMMON/SPDATA/AA(90,5),XMF(90),XMW(90),SIGMA(90),OMEGA(90),TR,N
      COMMON/SPNAME/SPNAM1(90),SPNAM2(90),TEMP( 5, 90),IDATA,KK,KT
      COMMON/THRMTR/A(90,15)
      COMMON/MO/NUM(90)
      COMMON/COUNT/IKLUG
      DATA(TEND(I),I=1,4)/4*6HEND    /
      DATA(TITLE(I),I=1,4)/6HSPECIE,6HDATA F,6HOR TRA,6HNSPROP/
      IF(IFIRST.EQ.0.AND.J.EQ.3) GO TO 6
      IF(J.GT.3) GO TO 90
      IF(IFIRST.EQ.1)GO TO 10
      IF(IKLUG.GT.0)GO TO 6
      IKLUG=1
      IF(IFLG1.EQ.0)GO TO 191
      WRITE(6,3)
3  FORMAT(39HOB ARRAY CONTAINING SOME DATA FOR TRANS)
      WRITE(6,4)((B(I,JD),I=1,5),JD=1,KD)
4  FORMAT(5X,2A6,3E10.3)
191 CONTINUE
6  CONTINUE
      IFIRST = 1
      DO 9 KRD=1,KD
      DO 15 I=1,5
15  DDD(KRD,I)=B(I,KRD)
9  CONTINUE
10  CONTINUE
      KK=0
      KRD=KD
      DO 25 I=1,KRD
      DO 17 III=1,5

```

```

17 D(III) = DDD(1,III)
   DO 20 JJ =8, IDATA
   IF ( D(1).EQ.TEMP(1,JJ))GO TO 11
   GO TO 20
11 IF (D(2).EQ.TEMP(2,JJ))GO TO 21
20 CONTINUE
   GO TO 25
21 KK=KK+1
   NUM(KK) = JJ
   DO 22 L=1,5
22 A(KK,L)= D(L)
   IF (IFLG1.EQ.0)GO TO 192
   WRITE(6,200)
200 FORMAT(39HOA ARRAY CONTAINING GAS DATA TO BE USED)
   WRITE(6,201)KK,(A(KK,L),L=1,5)
201 FORMAT(4X,I2,2X,2A6,3F10.3)
192 CONTINUE
   IF(KK+7.EQ.IDATA) GO TO 50
25 CONTINUE
50 NUMFND = 0

C
C   FIND AND FILL IN THERMO DATA
C
51 READ(13) (D(I),I=1,5),((DD(I,IJ),I=1,9),IJ=1,2)
   IF(IFLG1.EQ.0)GO TO 193
   WRITE(6,500)(D(I),I=1,5)
500 FORMAT(23HOD ARRAY READ FROM TAPE,5E10.3)
193 CONTINUE
   DO 70 JJ=1,KK
   IF(D(1).EQ.TEND(1)) GO TO 80
   IF(D(1).NE.A(JJ,1)) GO TO 70
   IF(D(2).EQ.A(JJ,2)) GO TO 72
70 CONTINUE
   GO TO 51
72 LI =5
   DO 78 NN=1,2
   DO 77 LL=3,7
   LI=LI+1

```

```

77 A(JJ,LI) = DD(LL,NN)
78 CONTINUE
   IF(IFLG1.EQ.0)GO TO 194
   WRITE(6,202)D(1),D(2)
202 FORMAT(5X,2A6)
   WRITE( 6,203)((A(JJ,LI)*LI=6*15))
203 FORMAT(1H0, 10E10.3)
194 CONTINUE
   NUMFND = NUMFND+1
   IF(NUMFND.EQ.KK) GO TO 90
   GO TO 51
80 IF(NUMFND.EQ.KK) GO TO 90
   WRITE(6,81)
81 FORMAT(1H0,50HNOT ALL SPECIES FOUND ON THERMO-CHEM PRODUCT TAPE )
90 N=0
   M = 1
   REWIND 13
91 DO 96 NN=1,KK
   IF(SPNAM1(M).NE.A(NN,1)) GO TO 96
   IF(SPNAM2(M).EQ.A(NN,2)) GO TO 98
   GO TO 96
98 TK = TR/1.8
   N = N + 1

C
C** SET ARRAY CONTAINING CONSTANTS FOR GAS CALCULATIONS
C
   JJ=0
   IF(TK.GT.999.) GO TO 110
   DO 105 LL = 11,15
   JJ= JJ+1
105 AA(N,JJ) = A(NN,LL)
   GO TO 120
110 DO 115 LL = 6,10
   JJ=JJ+1
115 AA(N,JJ) = A(NN,LL)
120 NNB = NUM(NN)

C
C** MOLE FRACTIONS

```

```

      XMF(N) = TEMP(J,NN8)
      SPNAM1(N) = A(NN,1)
      SPNAM2(N) = A(NN,2)
C**  SPECIES MOLECULAR WEIGHT
      XMW(N) = A(NN,3)
      SIGMA(N)=A(NN,4)
      OMEGA(N)=A(NN,5)
      IF(IFLG1.EQ.0)GO TO 195
      WRITE(6,300)J,NN,NN8,TEMP(J,NN8)
300  FORMAT(10HONUM CHECK,2X,3I5,2X,E10.3)
195  CONTINUE
      GO TO 97
      96 CONTINUE
      97 IF (M .EQ. KK) GO TO 9999
      M = M + 1
      GO TO 91
9999 RETURN
      END

```

\$IBFTC BDATA DECK

BLOCK DATA

COMMON/DRAY/B(5,100),KD

DATA KD/45/

DATA ((B(I,J),I=1,5),J=1,19)/

| | | | | | | | | |
|-----------|------|---|--------|---|-------|---|--------|---|
| 16HAL | , 6H | , | 26.98 | , | 2.655 | , | 2750.0 | , |
| 26HALCL | , 6H | , | 62.444 | , | 3.578 | , | 972.0 | , |
| 36HALCL3 | , 6H | , | 133.55 | , | 5.127 | , | 472.0 | , |
| 46HALF | , 6H | , | 45.98 | , | 3.148 | , | 556.0 | , |
| 56HALF3 | , 6H | , | 83.98 | , | 4.198 | , | 1846.0 | , |
| 66HALN | , 6H | , | 40.99 | , | 3.369 | , | 2682.0 | , |
| 76HALO | , 6H | , | 42.98 | , | 3.204 | , | 542.0 | , |
| 86HALS | , 6H | , | 59.05 | , | 3.73 | , | 1526.0 | , |
| 96HAL2 | , 6H | , | 53.96 | , | 2.94 | , | 2750.0 | , |
| A6HAR | , 6H | , | 39.944 | , | 3.542 | , | 93.3 | , |
| B6HAS1H3 | , 6H | , | 77.94 | , | 4.145 | , | 259.8 | , |
| C6HB | , 6H | , | 10.82 | , | 2.265 | , | 3331.0 | , |
| D6HBBR3 | , 6H | , | 250.57 | , | 5.439 | , | 430.0 | , |
| E6HBCL | , 6H | , | 46.28 | , | 3.318 | , | 1026.0 | , |
| F6HBCL2 | , 6H | , | 81.73 | , | 4.222 | , | 682.0 | , |
| G6HBCL3 | , 6H | , | 117.19 | , | 5.127 | , | 337.7 | , |
| \$6HCCLF3 | , 6H | , | 104.47 | , | 4.96 | , | 188.0 | , |
| \$6HCF4 | , 6H | , | 88.01 | , | 4.662 | , | 121.0 | , |
| \$6HCHF3 | , 6H | , | 70.02 | , | 4.33 | , | 240.0/ | , |

DATA ((B(I,J),I=1,5),J=20,38)/

| | | | | | | | | |
|--------|------|---|--------|---|-------|---|-------|---|
| H6HCH4 | , 6H | , | 16.04 | , | 3.758 | , | 148.6 | , |
| I6HCO | , 6H | , | 28.01 | , | 3.690 | , | 91.7 | , |
| J6HCOS | , 6H | , | 60.08 | , | 4.13 | , | 336.0 | , |
| K6HC02 | , 6H | , | 44.01 | , | 3.941 | , | 195.2 | , |
| L6HCS | , 6H | , | 44.08 | , | 4.216 | , | 199.4 | , |
| M6HCL | , 6H | , | 35.457 | , | 3.613 | , | 130.8 | , |
| N6HCL2 | , 6H | , | 70.91 | , | 4.217 | , | 316.0 | , |
| O6HH | , 6H | , | 1.008 | , | 2.708 | , | 37.0 | , |
| P6HH2 | , 6H | , | 2.016 | , | 2.827 | , | 59.7 | , |
| Q6HHCL | , 6H | , | 36.47 | , | 3.339 | , | 344.7 | , |
| R6HH20 | , 6H | , | 18.02 | , | 2.641 | , | 809.1 | , |
| S6HHS | , 6H | , | 33.07 | , | 3.673 | , | 86.4 | , |
| T6HH2S | , 6H | , | 34.08 | , | 3.623 | , | 301.1 | , |

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| | | | | | | | | | |
|-------------------------------|---|----|---|--------|---|-------|---|--------|---|
| U6HN2 | , | 6H | , | 28.02 | , | 3.798 | , | 71.4 | , |
| V6HNH3 | , | 6H | , | 17.03 | , | 2.90 | , | 558.3 | , |
| W6HNO | , | 6H | , | 30.01 | , | 3.492 | , | 16.7 | , |
| \$6HN2O | , | 6H | , | 44.02 | , | 3.828 | , | 232.4 | , |
| *6HNE | , | 6H | , | 20.183 | , | 2.82 | , | 32.8 | , |
| X6HO | , | 6H | , | 16.0 | , | 3.05 | , | 106.7 | / |
| DATA((B(I,J),I=1,5),J=39,45)/ | | | | | | | | | |
| Y6HO2 | , | 6H | , | 39.0 | , | 3.467 | , | 106.7 | , |
| Z6HOH | , | 6H | , | 17.01 | , | 3.147 | , | 79.8 | , |
| *6HS | , | 6H | , | 32.066 | , | 3.839 | , | 847.0 | , |
| \$6HSF6 | , | 6H | , | 146.07 | , | 5.128 | , | 222.1 | , |
| *6HSO | , | 6H | , | 48.07 | , | 3.993 | , | 301.0 | , |
| *6HSO2 | , | 6H | , | 64.07 | , | 4.112 | , | 335.4 | , |
| *6HS2 | , | 6H | , | 64.13 | , | 4.519 | , | 847.0/ | |
| END | | | | | | | | | |

\$*

\$ORIGIN B


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$IBFTC SOUR    DECK
      SUBROUTINE SOURCE(IDUM,ISCON)
      COMMON/WRIT/IFLG1
      DIMENSION SAVEA(16)
      DATA (SAVEA(K),K=1,16) /16*0./
      99 FORMAT(1H1)
      100 FORMAT(4X2HS2,7X7HMACH N05X5HRE N05X7H GAMMA 2X10HKNUDSEN N05X,3H
      1T05X1HT9X2HP010X1HP)
      200 FORMAT(1H0,10E11.4,2X,13)
      300 FORMAT(1H020X,32HVIBRATIONAL ENERGY MODE FROZEN)
      400 FORMAT(1H052X,32HR0TATIONAL ENERGY MODE FROZEN)
      500 FORMAT(1H084X,32HTRANSLATIONAL ENERGY MODE FROZEN)
      COMMON/PLUMF2/PROP(10,200),IPT
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/GASCON/GAMA,R,T0,PO,EM,RHO,T,WM ,Q
      COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
      COMMON/LIP/THET,PI02
      COMMON/EXCON/PEX,EMU
      COMMON/TAPE/IPROT
      EQUIVALENCE(GAMA,GAMMA)
      IPT=0
      IFREZ=0
      ITC1=0
      ITC2=0
      LPAGE=1
      POWER=.95
      CNLOCL=0.
      GMT=1.4
      ISCON=0
      PI=3.1415926536
      PI02=PI/2.
      REXT=RADTHT*SQRT(AEOAT)
      C FIRST COMPUTE LIP EXPANSION ANGLE
      RE=RADTHT*SQRT(AEOAT)
      ANGLP=ANGLP/57.29578
      P=PEX
      CALL TABLE(P,1)
      QE=Q

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```

      RHOEX=RHO
      WRITE(6,1022)P ,EM,GAMA,RHOEX,QE
1022 FORMAT(10HOEXIT PROP,5E10.3)
      EM1=EM
      VNU=PI02*(SQRT((GAMA+1.)/(GAMA-1.))-1.)
      VN1= SQRT((GAMA+1.)/(GAMA-1.))*ATAN(SQRT((GAMA-1.)/(GAMA+1.))
      *(EM*EM-1.))-ATAN(SQRT(EM*EM-1.))
      DELTHT=VNU-VN1
      THET=DELTHT+ANGLP
      WRITE(6,9000)GAMA,VNU,THET
9000 FORMAT(6HOGAMA=E10.3,4HVNU=E10.3,5HTHET=E10.3)
C     TEST IF THET GT 90.
      IF(THET.GE.PI02)GO TO 5
      X=-RE/TAN(THET)
      GO TO 15
      5 CONTINUE
      IF(THET.EQ.0.)GO TO 10
      THT=THET-PI02
      WRITE(6,9001)THT
9001 FORMAT(5HOTHT=E10.3)
      X=RE*TAN(THT)
      GO TO 15
      10 X=0.
      15 CONTINUE
      WRITE(6,904)X,THET
904  FORMAT(1H027HORIGIN OF SOURCE FLOW AT X=.E10.3,5X,11HWITH THETA=,E
110.3)
      P1=P
      P2=P
      P01=TAB(1,5,1)
      T01=TAB(1,6,1)
      FUG=2.*THET
      FUG =2.*PI*(1.-COS(THET))
      PSTAR=TAB(1,5,2)
      CALL TABLE(PSTAR,1)
      RSTAR=RHO
      QSTAR=Q
      WFSTAR=RSTAR*QSTAR*AT

```

```

WRITE(6,1023)WFSTAR,RSTAR,QSTAR
1023 FORMAT(1H0,11HTHROAT PROP,3E10.3)
WRITE(6,99)
WRITE(6,100)
SREF =2.*RE
SST = .25
IF(IPROT.EQ.1)SST=1.0
S1=X
S2 =0.
AEXT = AT*AEOAT
585 S2 = S2 + SST
SSQR = FUG*S2*S2
IF(SSQR.LE.AEXT)GO TO 585
S2 = S2 +SREF
PINC=-.09*P
17 CONTINUE
SAVEA(2)=PINC
SAVEA(1)=1.0
TOL=.05*WFSTAR
C THIS SECTION COMPUTES GAS PROPERTIES UNTIL FREEZING DETECTED
C
18 CONTINUE
IF(P2.LE.0.)GO TO 32
GO TO 37
32 CONTINUE
P2=P2-.95*PINC
PINC=.1*PINC
SAVEA(2)=PINC
37 CONTINUE
IF(CNLOCL.GT.1./500.)GO TO 19
C USE P TO CALL TABLE
CALL TABLE(P2,1)
GO TO 89
19 POP=P2/P0
RGK=1545.*32.174/TAB(1,7,1)
T=T0*(P2/P0)**((GAMA-1.)/GAMA)
TOVT=T0/T
SOS=SQRT(GAMA*RGK*T)

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      FM=SQRT((TOVT-1.)/((GAMA-1.)/2.))
      Q=EM*SOS
      RHO=P2*32.174/(T*RGK)
89  CONTINUE
      WF2=WFDOT(P2,RHO,Q,THFT,S2)
      FP=WFSTAR-WF2
      GO TO 1776
      WRITE(6,91)WF2,P2,RHO,Q,S2,GAMA,EM,T
91  FORMAT(1H0,4HWF2=E10.3,3HP2=E10.3,4HRHO=E10.3,2HQ=E10.3,3HS2=E10.3
      S,5HGAMA=E10.3,3HEM=E10.3,2HT=E10.3)
      WRITE(6,92)SAVEA(2),PINC
92  FORMAT(1H0,5HSAVE=E10.3,5HPINC=E10.3)
      WRITE(6,50)TOL
50  FORMAT(5X,4HTOL=,E10.3)
1776 CONTINUE
      CALL ITSUB(FP,P2,SAVEA,TOL,199)
      II=SAVEA(1)+.1
      NI=SAVEA(3)+.1
      GO TO (18,18,18,18,22,23),II
23  WRITE(6,600)S2 ,P2,FP
600 FORMAT(24H0ITSUB WILL NOT CONVERGE,1X,5HS2 =,E12.5,1X,2HP=,E12.5,
      11X,3HFP=,E12.5)
      I$CON=1
      GO TO 40
22  CONTINUE
      PINC=.09*P2
4500 FORMAT(8H0CNLOCL=E10.3)
      DS=S2-S1
C    EM1 SAVED FROM PREVIOUS POINT CALCULATION
70  CONTINUE
      EM2=EM
80  CONTINUE
      GP102=(GAMA+1.)/2.
      ONOGM1=1./((GAMA-1.))
      ROUSTR=P0/(R*T0)*((GP102**(-ONOGM1)))*SQRT(2.0*GAMMA*R*T0/(GAMMA+
      S1.0))
      T02=T0
      SBAR=(S2+S1)/2.

```

```

EMBAR=(EM1+EM2)/2.
VIS=1.36E-9*(T/1.8)**POWER
RE=ROUSTR/(VIS*SBAR**2)
DLOGT=ALOG(T02/T01*(2.+(GAMMA-1.)*EM1**2)/(2.+(GAMMA-1.)*EM2**2))
DLTDS=ABS(DLOGT/DS)
CNLOCL=(2.51*3.14*GAMMA)*((EMBAR*EMBAR)/RE)*DLTDS
IF(LPAGE.LT.55)GO TO 55
LPAGE=1
WRITE(6,99)
WRITE(6,100)
55 CONTINUE
WRITE(6,200) S2,EM2,RE,GAMMA,CNLOCL,T0,T,P0,P2
LPAGE=LPAGE+2
IPT=IPT+1
C THE FOLLOWING STATEMENTS STORE PLUME PROPERTIES IN PROP ARRAY
PROP(1,IPT)=S2/(2.*REXT)
PROP(2,IPT)=SSQR
PROP(3,IPT)=GAMA
PROP(4,IPT)=EM2
PROP(5,IPT)=P2
PROP(6,IPT)=T
PROP(7,IPT)=WM
GO TO 30
IF(CNLOCL.LT.1./500.)GO TO 30
IFREZ=1
C CALCULATION WITH VIBRATIONAL ENERGY MODE FROZEN
GAMMA=1.4
GM1O2=(GAMMA-1.)/2.
ONOGM1=1./(GAMMA-1.)
GOGM1=GAMMA*ONOGM1
ITC1=ITC1+1
IF(ITC1.EQ.1)T0=T*(1.+GM1O2*EM2*EM2)
P0=P2*(T0/T)**GOGM1
WRITE(6,300)
IF(CNLOCL.LT.1./5. )GO TO 30
C CALCULATION WITH VIBRATIONAL AND ROTATIONAL ENERGY MODE FROZEN
PINC=.07*P2
CK=CNLOCL

```

```

GAMMA= -.000567*CK**3 +.00868*CK**2 -.003404*CK +1.4003
IF(CNLOCL.GE.10.)GAMMA=1.667
ONOGM1=1./(GAMMA-1.)
GOGM1=GAMMA*ONOGM1
GM1O2=(GAMMA-1.)/2.
IF(GAMMA.LE.1.667)T0=T*(1.+GM1O2*EM2*EM2)
P0=P2*(T0/T)**GOGM1
WRITE(6,400)
IF(CNLOCL.LT..8)GO TO 30
C   CALCULATION WITH VIBRATIONAL,ROTATIONAL AND TRANSLATIONAL ENERGY
C   MODE FROZEN
WRITE(6,500)
30 EM1=EM2
   T01=T02
   S1=S2
   STRECH=1.0
   DELTS=SREF
   S2=S2+DELTS
   IF(EM2.GE.100.)GO TO 40
   IF(IPT.GE. 75)GO TO 40
   GO TO 17
40 CONTINUE
   RETURN
   END

```

```

$IBFTC WDOT1  DECK
      FUNCTION WFDOT(P0,R0,Q0,THTM,R)
      PI=3.14159265
      TWOPI=2.*PI
      PIO2=PI/2.
C
      DELTHT=THTM/20.
      THETA=0.
      AREA=0.
      DO 20 J=1,20
      I1=J
      I2=J+1
      THETA=THETA
      CR=(COS(PIO2*THETA/THTM))**7
      CV=1.
      SA=SIN(THETA)
      F1 =CR*CV*SA
      THETA=THETA+DELTHT
      CR=(COS(PIO2*THETA/THTM))**7
      CV=1.
      SA=SIN(THETA)
      F2 =CR*CV*SA
      A=.5*DELTHT*(F1+F2)
20  AREA=AREA+A
      WFDOT=TWOPI*R0*Q0*R**2*AREA
      RETURN
      END

```

```

$IBFTC ADJUST
  SUBROUTINE ADJUST(      NOK,KAZE)
  COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DELM,DELMN,
$DELREY
  COMMON/AVE/EMM,EMWM,HM,HOM,GM,SLP1,SLP2
  COMMON/GASES/TAB(3,12,13),NMIX
  COMMON/CHAMB/PCHAMI,TCHAMI,PMAX,TMAX
  COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
  COMMON/PLUMF1/PRPR(10,4),REYPLM
  COMMON/MOLWT/SA,SB,SC
  COMMON/REGION/XC11,XC12,XC13,ERRMAX,ITYPE
  COMMON/EXCON/PEX,EMU
  COMMON/GEOM/AT,RADTHT,AEOAT,ANGLP,REYNP
  LOGICAL KAZE
  PIO2=3.1415927/2.0
  NOK=0
  GO TO(300,310,320),ITYPE
300 CONTINUE
C   COMPUTE MACH NO. CHANGE FOR MOMENTUM FLUX ERROR
  P=PC(2)
  G=GMC(2)
  DEM = SQRT(ABS(DELM)/(P*G))
  IF(DELM.LT.0.) SIGN = -1.0
  IF(DELM.GT.0.) SIGN = +1.0
  DEM = SIGN*DEM
  GO TO 340
310 CONTINUE
  DEM=DELM
  GO TO 340
320 CONTINUE
C   COMPUTE MACH NO. CHANGE FOR REYNOLDS NO. ERROR
  GO2= (GMC(2)-1.)/2.
  EMF= (1.+GO2*EMC(2)*EMC(2))
  EGX=-1.*(3.*GMC(2)-1.)/(2.*(GMC(2)-1.))
  R=1545.*32.174/EMWC(2)
  D= 2.*RADTHT*SQRT(AEOAT)
  VISCOS=1.36E-09*(T/1.8)**.95
  PTL= PCHAMI*SQRT(GMC(2)/(R*TCHAMI))*D/VISCOS

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      DEM=DELRELY/(PTL*(EMF)**EGX+EMC(2)*EMC(2)*EGX*EMF**(EGX-1.)*(GMC(2)-1.))
      $-1.))
340 CONTINUE
      KAZE=.FALSE.
C      COMPUTE MEAN PROPERTIES FOR GAS MIXTURE UNDERGOING TESTING
      CALL MEAN(DEM,P)
C      COMPUTE CHANGE FOR MOLECULAR WT.
      HOH=HM/HOM
      SH=SLP1/HM
      GM2=(GM-1.)/2.
      ONOM=1./EMWM
      GF1=SQRT((GM-1.)/(GM+1.))
      GF2=1./(GM-1.)**2
      AG=PI02*GF1*GF2/THET
      DELMW=(2.*DEM/EMM)/(ONOM+2.*HOH*(-SH+GM2*EMM**2*(SH-ONOM)+SLP2*
1AG)+2.*SH-2.*ONOM-2.*SLP2*AG-SLP2/GM-SLP1/HM)
      DELMW=-1.0*DELMW
      WRITE(6,5)DELMW
5      FORMAT(33H0COMPUTED CHANGE IN MOLECULAR WT=,E10.3)
      WMN=TAB(1,7,1)+DELMW
      CHCK=TAB(2,7,1)/TAB(3,7,1)
      IF(CHCK.GT.1.)GO TO 150
      WM1=TAB(2,7,1)
      WM2=TAB(3,7,1)
150 WM1=TAB(3,7,1)
      WM2=TAB(2,7,1)
160 CONTINUE
C      TEST IF DELMW POSSIBLE
      IF(1.05*WM1.GT.WMN)GO TO 50
      IF(.95*WM2.LT.WMN)GO TO 70
      IF(NMIX.EQ.3)GO TO 20
      X1P=SA*(SB/WMN-1.)/(SB-SA)
      X2P=1.-X1P
      WRITE(6,10)X1P,X2P
10      FORMAT(30H0NEW MIXTURE RATIOS ARE, X1P=,E10.3,2X,4HX2P=,E10.3)
C      BINARY MIXTURE
      PC21=X1P
      PC22=X2P

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```

        IF(X1P.LE.0..OR.X2P.LE.0.)GO TO 30
        TNW=TAB(1,6,1)/1.8
        PNW=TAB(1,5,1)/144.
        GO TO 200
C      IF NEW MIXTURE PHYSICALLY IMPOSSIBLE • COME HERE
30     CONTINUE
        WRITE(6,31)X1P,X2P
31     FORMAT(5X,4HX1P=,E10.3,5X,4HX2P=,E10.3,5X,19HCHANGE BINARY GASES)
        KAZE=.TRUE.
        NOK=1
        GO TO 110
20     CONTINUE
C      TERNARY MIXTURES
        FC=PC33
        FA=(1.-FC*WMN/SC-(1.-FC)*WMN/SB)/(WMN/SA-WMN/SB)
        FB= 1.-FC-FA
        X1=FA
        X2=FB
        WRITE(6,15)X1,X2,PC33
15     FORMAT( 28HNEW MIXTURE RATIOS ARE, X1=,E10.3,2X,3HX2=,E10.3,
12X,3HX3=,E10.3)
C      TEST IF PHYSICALLY POSSIBLE
        IF(X1.LT.0.)GO TO 80
        IF(X2.LT.0.)GO TO 80
        PC31=X1
        PC32=X2
        PNW=TAB(1,5,1)/144.
        TNW=TAB(1,6,1)/1.8
        GO TO 200
50     CONTINUE
        WRITE(6,51)WMN
51     FORMAT(5X,4HWMN=E10.3,38HNEW MW LT MIN.,ADJUST PRESSURE      DOWN)
        RATIO = PRPR(5,2)/PC(2)
        PNW= TAB(1,5,1)*RATIO/144.
        TNW =  TAB(1,6,1)/1.8
        IF(PNW.LT.0.)GO TO 100
        GO TO 200
70     CONTINUE

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        WRITE(6,71)WMN
71  FORMAT(5X,4HWMN=E10.3,36HNEW MW GT MAX.,ADJUST PRESSURE      UP)
        RATIO = PRPR(5,2)/PC(2)
        PNW= TAB(1,5,1)*RATIO/144.
        TNW = TAB(1,6,1)/1.8
        IF(PNW.GT.PMAX)GO TO 105
        GO TO 200
80  CONTINUE
        WRITE(6,81)X1,X2
81  FORMAT(5X,3HX1=,E10.3,5X,3HX2=,E10.3,5X,12HCHANGE GASES)
        GO TO 110
C    FLAGS SET IN THIS SECTION TO CHANGE GASES
100  CONTINUE
        WRITE(6,101)
101  FORMAT(13HOPLOW REACHED)
        KAZE=,TRUE.
        PNW=PCHAMI
        TNW=TCHAMI
        NOK=1
        GO TO 200
105  CONTINUE
        WRITE(6,106)
106  FORMAT(13HOP HI REACHED)
        KAZE=,TRUE.
        PNW=PCHAMI
        TNW=TCHAMI
        NOK=1
        GO TO 200
110  CONTINUE
        PNW=PCHAMI
        TNW=TCHAMI
        NOK=1
        KAZE=,TRUE.
200  RETURN
        END
$IBFTC WTM01
        SUBROUTINE WTMOL(SA,SR,SC)
        COMMON/CHANGE/PC11,PC21,PC22,PC31,PC32,PC33,PNW,TNW,DELM,DELMN,

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$DELREY
COMMON/GASES/TAB(3,12,13),NMIX
DIMENSION A(20,3),B(3),C(3)
C LOAD QUANTITIES INTO ARRAYS
C COMPUTE MOLECULAR WTS OF INDIVIDUAL GASES
A(1,1)=PC31+PC32
A(1,2)=0.
A(1,3)=PC33
A(2,1)=0.
A(2,2)=PC31+PC32
A(2,3)=PC33
A(3,1)=PC31
A(3,2)=PC32
A(3,3)=PC33
CALL GASINV(A,3,DET)
B(1)= 1./TAB(2,7,1)
B(2)= 1./TAB(3,7,1)
B(3)= 1./TAB(1,7,1)
CALL MATMPY(A,B,C,3,3,1)
SA=1./C(1)
SB=1./C(2)
SC=1./C(3)
RETURN
END

```

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$IBFTC MEA1    DECK
  SUBROUTINE MEAN(DEM,P)
  COMMON/AVE/EMM,EMWM,HM,HOM,GM,SLP1,SLP2
  COMMON/ENDS/TE(2),G(2),HOE(2),HE(2),EME(2)
  COMMON/PLUNMU/XC(5),PC(5),EMC(5),GMC(5),TC(5),QC(5),EMWC(5)
  COMMON/GASES/TAB(3,12,13),NMIX
  CALL ENDPT(P)
C
C
C COMPUTE EXTRA PROPERTIES AT PLUME PT
  UGC=1545.
  RGC=UGC/EMWC(2)
  CP= GMC(2)*RGC/(GMC(2)-1.)
  H = CP*TC(2)
  HO= H+.5*QC(2)**2
C TEST ON DIRECTION OF CHANGE
C AND SET END POINT VALUES
  IF(DEM.GT.0.)GO TO 100
C NEGATIVE MACH NO. AND THUS MW CHANGE
  G1=G(1)
  HO1=HOE(1)
  H1=HE(1)
  EMW1=TAB(2,7,1)
  SLP1=(H-H1)/(EMWC(2)-EMW1)
  SLP2=(GMC(2)-G1)/(EMWC(2)-EMW1)
  EMM=(EME(1)+EMC(2))/2.0
  GM=(GMC(2)+G1)/2.0
  EMWM=(EMW1+EMWC(2))/2.0
  HM= (H1+H)/2.0
  HOM=(HO+HO1)/2.0
  GO TO 200
100 CONTINUE
  G1=G(2)
  HO1=HOE(2)
  H1=HE(2)
  EMW1= TAB(3,7,1)
  SLP1= (H-H1)/(EMWC(2)-EMW1)
  SLP2= (GMC(2)-G1)/(EMWC(2)-EMW1)
  EMM = (EME(1)+EMC(2))/2.0

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      EMWM= (EMW1+EMWC(2))/2.0
      HM=(H1+H)/2.0
      HOM=(HO+HO1)/2.0
      GM= (GMC(2)+G1)/2.0
200 CONTINUE
      IWRT=1
      IF(IWRT .EQ.0)GO TO 20
      WRITE(6,5)
      5 FORMAT(25H0MEAN PROPERTIES OF GASES)
      WRITE(6,10)
      10 FORMAT(10X,3HEMM,8X,4HEMWM,8X,2HHM,9X,3HHOM,8X,2HGM)
      WRITE(6,15)EMM,EMWM,HM,HOM,GM
      15 FORMAT(6X,5E10.3)
      20 CONTINUE
      RETURN
      END

```

```

$IBFTC ENDP1  DECK
SUBROUTINE ENDPT(P)
COMMON/ENDS/TE(2),G(2),HOE(2),HE(2),EME(2)
COMMON/GASCON/GAMA,R,T0,P0,EM,RHO,T,WM,Q
COMMON/ENTH/H
C SUBROUTINE COMPUTES GAS PROPERTIES OF INDIVIDUAL SPECIE GASES
C AT PRESSURE SPECIFIED
P1=P
DO 200 J=2,3
L=J-1
CALL TABLE(P1,J)
TE(L)=T
G(L)=GAMA
HE(L)=H
HOE(L)=H+.5*Q**2
EME(L)=EM
WRITE(6,10) P
10 FORMAT(48HOEND POINT PROPERTIES OF COMPOSITE AT PRESSURE= ,E10.3)
WRITE(6,11)
11 FORMAT(20X,3HGAS,6X,1HT,10X,1HH,10X,5HGAMMA,5X,1HM,10X,2HHO)
WRITE(6,12)L,T,H,GAMA,EM,HOE(L)
12 FORMAT(21X,I2,2X,6E10.3)
200 CONTINUE
100 RETURN
END

$*
$ORIGIN B

```

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LMSC/HREC D162424

```

$IBFTC CECS1  DECK
  SUBROUTINE CEC (LSD,KACE)
C
C 10
C TO LESSEN THE NO. OF CHANGES THAT MUST BE MADE, THE THERMODYNAMIC
C DATA FOR THE TRANSPORT PROPERTIES WILL BE READ FROM TAPE 12, THE
C OLD NASA/LEWIS DATA TAPE.
C THE THERMODYNAMIC DATA FOR THE CEC PORTION WILL BE READ FROM TAPE
C 8, THE NEW DATA TAPE GENERATED BY MCDERMIT.
C TO MAKE THESE COMPATABLE THE CEC IS MODIFIED TO READ THE GAS NAME
C UNDER A ZAG FORMAT.
C
C 30
C DOUBLE PRECISION G,X 40
C INTEGER DATA, OMIT, ENSERT, REAC, BLANK, THRM, END, SUB 50
C LOGICAL HP, SP, TP, IDEBUG, NEWR, IONS, MOLES, FROZ, EQL, PSIA, RKT 60
C LOGICAL SHOCK, MMHG, PASCAL, EV, IC, DETN, CPCVFR, CPCVEQ, SIUNIT, EUNITS 70
C 80
C INTEGER DATDUM
C DIMENSION DATDUM(5)
C COMMON/TAPE/IPROT
C COMMON/WRIT/IFLG1
C COMMON/GASES/TAB(3,12,13),NMIX
C COMMON/MOLFRC/ZFRAC(40),KFR
C DIMENSION OMIT(3,3),NCD(4),ENSERT(3,3),LH(2),LVP(2) ,LVM(2) 90
1  *WPSAVE(2) 100
C COMMON/SUNUP/SUN(3,40,2)
C COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13) 110
1  ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13) 120
2  *TOTN(13) 130
C COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150) 140
1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2) 150
C COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2) 160
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2) 170
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5) 180
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15) 190
4  ,RHOP,RMW(15),TLN 200
C COMMON /DOUBLE/ G(20,21), X(20) 210
C COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM 220
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ 230

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LMSC/HREC D16242A


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2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1      240
COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13) 250
1  ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SSO          260
COMMON/CASENO/LST
COMMON/PNT/KPT(4)

C
EQUIVALENCE (OMIT,ENLN),(ENSERT,EN(1,3)),(NLM,L)      270
C
DATA MIT/4HOMIT/,BLANK/1H /, PSIA/4HPSIA/,REAC/4HREAC/,IZ/2H00/      290
1  ,INPUT/4HINPU/,IE/1HE/,INSERT/4HINSE/,THRM/4HTHER/,END/3HEND/      300
DATA LH/4HH,CA,4HL/G /,LVP/2HV+,1H /,LVM/2HV-,1H /,NMLT/4HNAME/      320
DATA (DATDUM(I),I=1,5)/6HREAC  ,6HNAME  ,6H      ,6H      ,
16H      /

C
NAMELIST/INPT2/KASE,P,T,EQRAT,OF,FPCT,FA,TP,HP,SP,RKT      330
1,PSIA,MMHG,SHOCK,IONS,EV,V,DETN,CPCVFR,CPCVEQ,IDEBUG      340
2,SIUNIT,EUNITS      350
C
LST=LSD      360
KASE=KACE      370
TLOW = 0.      380
NEWR = .FALSE.      390
C
1 WRITE(6,400)      400
400 FORMAT(1H1)      410
DATA(1)=DATDUM(1)      420
203 CONTINUE
204 FORMAT(5(3A4,3X))      440
WRITE (6,2045)(DATA(I),I=1,15)      450
2045 FORMAT(1X,5(3A4,3X))      460
IF(DATA(1).EQ.REAC) GO TO 11      480
IF(DATA(1).EQ.INPUT.OR.DATA(1).EQ.NMLT) GO TO 210      510
IF(DATA(1).EQ.BLANK) GO TO 203      520
1023 WRITE(6,1024)      530
1024 FORMAT(40H0ERROR IN ABOVE CARD. IGNORE CONTENTS. )      540
GO TO 203      550
11 CONTINUE
NOMIT=0

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LMSC/HREC D162424

| | | |
|---|--|------|
| | INSERT = 0 | 570 |
| | MOLES = .FALSE. | 580 |
| | CALL REACT | 590 |
| | DATA(1)=DATDUM(2) | |
| | WPSAVE(1) = WP(1) | 600 |
| | WPSAVE(2) = WP(2) | 610 |
| | IF(L.EQ.() WRITE(6,52) | 620 |
| | 52 FORMAT(24HOERROR IN REACTANT CARDS) | 630 |
| | GO TO 203 | 640 |
| C | | 650 |
| C | | 890 |
| C | | 1120 |
| C | BEGIN NAMELIST INPT2 | 1130 |
| C | | 1140 |
| | 210 DO 300 I=1,26 | 1150 |
| | V(I) = 0. | 1190 |
| | 300 CONTINUE | 1200 |
| | DO 307 I=2,26 | |
| | P(I)=0.0 | |
| | 307 T(I)=0.0 | |
| C | SET PRESSURE RATIO ARRAY | |
| | PCP(1)=1.0 | |
| | PCP(2)=25.0 | |
| | PCP(3)=300.0 | |
| | PCP(4)=1000.0 | |
| | PCP(5)=2000.0 | |
| | PCP(6)=3000.0 | |
| | PCP(7)=4000.0 | |
| | PCP(8)=5000.0 | |
| | PCP(9)=7000.0 | |
| | PCP(10)=10000. | |
| | PCP(11)=30000. | |
| | PCP(12)=60000. | |
| | PCP(13)=100000. | |
| C | | |
| | DO 308 I=14,26 | |
| | 308 PCP(I)=0.0 | |
| | V1 = 0. | 1210 |

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| | |
|--|------|
| V2 = 0. | 1220 |
| RHOP = 0. | 1230 |
| RKT=.TRUE. | |
| HP=.FALSE. | 1260 |
| SP=.FALSE. | 1270 |
| TP=.TRUE. | |
| IF(IPROT.EQ.1)TP=.FALSE. | |
| CPCVFR = .FALSE. | 1290 |
| CPCVEQ = .FALSE. | 1300 |
| SHOCK = .FALSE. | 1310 |
| DETN = .FALSE. | 1320 |
| EV = .FALSE. | 1330 |
| PASCAL = .FALSE. | 1340 |
| MMHG = .FALSE. | 1350 |
| PSIA=.TRUE. | |
| R = 1.987165 | 1370 |
| RR = 4184.*R | 1380 |
| SIUNIT = .FALSE. | 1390 |
| EUNITS = .FALSE. | 1400 |
| IONS = .FALSE. | 1410 |
| IDEBUG=.FALSE. | |
| IF(IFLG1.EQ.1)IDEBUG=.TRUE. | |
| FA = 0. | 1430 |
| OF = 0. | 1440 |
| EQRAT= 0. | 1450 |
| FPCT= 0. | 1460 |
| EQL = .TRUE. | 1470 |
| DO 305 I=1,26 | 1490 |
| IF(P(I),EQ.0.) GO TO 322 | 1500 |
| NP = I | 1510 |
| IF (MMHG) P(NP) = P(NP)/760. | 1520 |
| IF (PASCAL) P(NP) = P(NP)/101325. | 1530 |
| IF(PSIA) P(NP)=P(NP)/14.696006 | 1540 |
| 305 CONTINUE | 1550 |
| 322 IF (FA.NE.0.) OF = 1./FA | 1560 |
| IF(EQRAT.EQ.0.) GO TO 725 | 1570 |
| OF= (-EQRAT*VMIN(2)-VPLS(2))/(VPLS(1)+EQRAT*VMIN(1)) | 1580 |
| GO TO 727 | 1590 |

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| | | |
|------|--|------|
| 725 | IF(OF.NE.0.) GO TO 727 | 1600 |
| | IF(FPCT.EQ.0.) GO TO 9051 | 1610 |
| | OF= (100.-FPCT)/FPCT | 1620 |
| | GO TO 727 | 1630 |
| 9051 | WRITE(6,724) | 1640 |
| 724 | FORMAT(48HONO INPT2 VALUE GIVEN FOR OF, EQRAT, FA, OR FPCT) | 1650 |
| | IF(WP(2).NE.0.) OF=WPSAVE(1)/WPSAVE(2) | 1660 |
| 727 | WP(1) = OF | 1670 |
| | WP(2) = 1. | 1680 |
| | SUM = WP(1)+WP(2) | 1690 |
| | FPCT = 100.*WP(2)/SUM | 1700 |
| | IF (EQRAT.NE.0.) GO TO 746 | 1710 |
| | V2 = (WP(1)*VMIN(1)+WP(2)*VMIN(2))/SUM | 1720 |
| | V1 = (WP(1)*VPLS(1)+WP(2)*VPLS(2))/SUM | 1730 |
| | IF(V2.NE.0.) EQRAT=ABS(V1/V2) | 1740 |
| 746 | DO 747 I=1,L | 1750 |
| | B0(I) = (WP(1)*BOP(I,1)+WP(2)*BOP(I,2))/SUM | 1760 |
| 747 | CONTINUE | 1770 |
| | IF (EQRAT.EQ.1.) EQRAT= 1.000005 | 1780 |
| | IF(.NOT.IONS.OR.LLMT(L).EQ.IE) GO TO 748 | 1790 |
| | L = L+1 | 1800 |
| | LLMT(L) = IE | 1810 |
| | B0(L) = 0. | 1820 |
| 748 | HSUB0 = (WP(1)*HPP(1)+WP(2)*HPP(2))/SUM | 1830 |
| | IF(NEW) CALL SEARCH | 1840 |
| | DO 755 N=1,NREAC | 1850 |
| | IF(NAME(N,5).NE.IZ) GO TO 755 | 1860 |
| | TT = RTEMP(N) | 1870 |
| | CALL HCALC | 1880 |
| | GO TO 760 | 1890 |
| 755 | CONTINUE | 1900 |
| | IF(IFLG1.EQ.0)GO TO 291 | |
| 760 | WRITE(6,INPT2) | 1910 |
| | WRITE (6,770) | 1920 |
| 770 | FORMAT (1H0,17X,4HFUEL ,13X,7HOXIDANT ,12X,7HMIXTURE //) | 1930 |
| 780 | FORMAT (1H 2A4,3E18.8/) | 1940 |
| | WRITE (6,780) LH,HPP(2),HPP(1),HSUB0,LVP,VPLS(2),VPLS(1),V1, | 1950 |
| | 1LVM,VMIN(2),VMIN(1),V2 | 1960 |

| | | |
|-----|---|------|
| 291 | CONTINUE | 1970 |
| | HSUB0 = HSUB0/R | 1980 |
| | WRITE (6,785) | 1990 |
| 785 | FORMAT (8H ATOMS/G) | 2000 |
| | WRITE(6,780)(LLMT(1),BLANK,BOP(1,2),BOP(1,1),B0(1),I=1,L) | 2010 |
| | RHOP = WP(2)*RHO(1)+WP(1)*RHO(2) | 2020 |
| | IF(RHOP.NE.0.) RHOP = (WP(1)+WP(2))*RHO(1)*RHO(2)/RHOP | 2030 |
| | IQ1= L+1 | 2040 |
| | IF(NC.EQ.0) GO TO 790 | 2050 |
| | DO 302 J=1,NS | 2060 |
| | IF(IUSE(J).EQ.0) GO TO 302 | 2070 |
| | IF(IUSE(J).GT.0) IUSE(J)= -IUSE(J) | 2080 |
| | IF(NSERT.EQ.0) GO TO 302 | 2090 |
| | DO 301 I=1,NSERT | 2100 |
| | IF(SUB(J,1).NE.ENSERT(1,I)) GO TO 301 | 2110 |
| | IF(SUB(J,2).NE.ENSERT(2,I)) GO TO 301 | 2120 |
| | IF(SUB(J,3).NE.ENSERT(3,I)) GO TO 301 | 2130 |
| | ENSERT(1,I) = 0. | 2140 |
| | IQ1= IQ1+1 | 2150 |
| | IUSE(J)= -IUSE(J) | 2160 |
| 301 | CONTINUE | 2170 |
| 302 | CONTINUE | 2180 |
| | NSERT = 0 | 2190 |
| 790 | ITN= 35 | 2200 |
| | IC = .FALSE. | 2210 |
| | PP = NS | 2220 |
| | NPT = 1 | 2230 |
| | ENN = .1 | 2240 |
| | SUMN = ENN | 2250 |
| | XI = NS - NC | 2260 |
| | XI = FNN/XI | 2270 |
| | XLN = ALOG(XI) | 2280 |
| | DO 432 J=1,NS | 2290 |
| | IF(IUSE(J).EQ.-10000) IUSE(J)=0 | 2300 |
| | EN(J,1) = 0. | 2310 |
| | ENLN(J)=0. | 2320 |
| | IF (IUSE(J).NE.0) GO TO 432 | 2330 |
| | EN(J,1) = XI | |

| | | |
|-----|---------------------|------|
| | ENLN(J) = XLN | 2340 |
| 432 | CONTINUE | 2350 |
| | JSOL = 0 | 2360 |
| | JLIQ = 0 | 2370 |
| | IF(RKT) CALL ROCKET | 2390 |
| | KPT(LST)=NPT | |
| | RETURN | |
| | END | 2430 |

\$IBFTC CECS18 DECK
BLOCK DATA

| | | | | | | | | | |
|---|---|---|------------|--|--|--|--|--|-----|
| C | | | | | | | | | 10 |
| | | | | | | | | | 20 |
| C | | DIMENSION | ATEM(3,50) | | | | | | 30 |
| | | | | | | | | | 40 |
| C | | COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2) | | | | | | | 50 |
| | 1 | ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2) | | | | | | | 60 |
| | 2 | ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5) | | | | | | | 70 |
| | 3 | ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15) | | | | | | | 80 |
| | 4 | ,RHOP,RMW(15),TLN | | | | | | | 90 |
| C | | EQUIVALENCE (ATOM(1,52),ATEM) | | | | | | | 130 |
| | | | | | | | | | 140 |
| C | | | | | | | | | 150 |
| C | | ATOMIC SYMBOLS, WEIGHTS, AND VALENCES | | | | | | | 160 |
| | | | | | | | | | 170 |
| C | | DATA ATOM/ | | | | | | | 180 |
| | A | 2HH , 1.00797 , 1., 2HHE, 4.0026, 0., 2HLI, 6.939 , 1., | | | | | | | 190 |
| | B | 2HBE, 9.0122 , 2., 2HB , 10.811 , 3., 2HC , 12.01115, 4., | | | | | | | 200 |
| | C | 2HN , 14.0067 , 0., 2HO , 15.9994,-2., 2HF , 18.9984 , -1., | | | | | | | 210 |
| | D | 2HNE, 20.183 , 0., 2HNA, 22.9898, 1., 2HMG, 24.312 , 2., | | | | | | | 220 |
| | E | 2HAL, 26.9815 , 3., 2HSI, 28.086 , 4., 2HP , 30.9738 , 5., | | | | | | | 230 |
| | F | 2HS , 32.064 , 4., 2HCL, 35.453 , -1., 2HAR, 39.948 , 0., | | | | | | | 240 |
| | G | 2HK , 39.102 , 1., 2HCA, 40.080 , 2., 2HSC, 44.956 , 3., | | | | | | | 250 |
| | H | 2HTI, 47.900 , 4., 2HV , 50.942 , 5., 2HCR, 51.996 , 3., | | | | | | | 260 |
| | I | 2HMN, 54.9380 , 2., 2HFE, 55.847 , 3., 2HCO, 58.9332 , 2., | | | | | | | 270 |
| | J | 2HNI, 58.710 , 2., 2HCU, 63.540 , 2., 2HZN, 65.370 , 2., | | | | | | | 280 |
| | K | 2HGA, 69.720 , 3., 2HGE, 72.590 , 4., 2HAS, 74.9216 , 3., | | | | | | | 290 |
| | L | 2HSE, 78.960 , 4., 2HBR, 79.909 , -1., 2HKR, 83.800 , 0., | | | | | | | 300 |
| | M | 2HRB, 85.47 , 1., 2HSR, 87.620 , 2., 2HY , 88.905 , 3., | | | | | | | 310 |
| | N | 2HZR, 91.220 , 4., 2HNB, 92.906 , 5., 2HMO, 95.94 , 6., | | | | | | | 320 |
| | O | 2HTC, 99.000 , 7., 2HRU, 101.070 , 3., 2HRH, 102.905 , 3., | | | | | | | 330 |
| | P | 2HPD, 106.400 , 2., 2HAG, 107.870 , 1., 2HCD, 112.400 , 2., | | | | | | | 340 |
| | Q | 2HIN, 114.820 , 3., 2HSN, 118.690 , 4., 2HSB, 121.750 , 3. / | | | | | | | 350 |
| | | DATA ATEM/ | | | | | | | 360 |
| | R | 2HTE, 127.600 , 4., 2HI , 126.9044, -1., 2HXE, 131.300 , 0., | | | | | | | 370 |
| | S | 2HCS, 132.905 , 1., 2HBA, 137.340 , 2., 2HLA, 138.910 , 3., | | | | | | | 380 |
| | T | 2HCE, 140.120 , 3., 2HPR, 140.907 , 3., 2HND, 144.240 , 3., | | | | | | | 390 |
| | U | 2HPM, 145.000 , 3., 2HSM, 150.350 , 3., 2HEU, 151.960 , 3., | | | | | | | 400 |

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| | | | | | | | |
|---|--------------|-------|--------------|-------|--------------|-------|-----|
| V | 2HGD,157.250 | , 3., | 2HTB,158.924 | , 3., | 2HDY,162.500 | , 3., | 410 |
| W | 2HHO,164.930 | , 3., | 2HER,167.260 | , 3., | 2HTM,168.934 | , 3., | 420 |
| X | 2HYB,173.040 | , 3., | 2HLU,174.997 | , 3., | 2HHF,178.490 | , 4., | 430 |
| Y | 2HTA,180.948 | , 5., | 2HW ,183.850 | , 6., | 2HRE,186.200 | , 7., | 440 |
| Z | 2HOS,190.200 | , 4., | 2HIR,192.200 | , 4., | 2HPT,195.090 | , 4., | 450 |
| A | 2HAU,196.967 | , 3., | 2HHG,200.590 | , 2., | 2HTL,204.370 | , 1., | 460 |
| B | 2HPB,207.190 | , 2., | 2HBI,208.980 | , 3., | 2HPO,210.000 | , 2., | 470 |
| C | 2HAT,210.000 | , 0., | 2HRN,222.000 | , 0., | 2HFR,223.000 | , 1., | 480 |
| D | 2HRA,226.000 | , 2., | 2HAC,227.000 | , 3., | 2HTH,232.038 | , 4., | 490 |
| E | 2HPA,231.000 | , 5., | 2HU ,238.030 | , 6., | 2HNP,237.000 | , 5., | 500 |
| F | 2HPU,242.000 | , 4., | 2HAM,243.000 | , 3., | 2HCM,247.000 | , 3., | 510 |
| G | 2HBK,249.000 | , 3., | 2HCF,251.000 | , 3., | 2HES,254.000 | , 0., | 520 |
| H | 2HFM,253.000 | , 0., | 2HMV,256.000 | , 0./ | | | 530 |
| | END | | | | | | 740 |

\$*


```

$IBFTC CECS13  DECK
C
SUBROUTINE ROCKET
C
ROCKET PERFORMANCE
C EITHER HPSP OR TPSP IS TRUE
C
LOGICAL HP,SP,TP,IDEBUG,NEWR ,IONS,MOLES,FROZ,EQL,LOGV,HPSP,TPSP
C
DIMENSION AA(2),BB(2),CC(2)
C
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2 ,TOTN(13)
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)
1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4 ,RHOP,RMW(15),TLN
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1 ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0
COMMON/CASENO/LST
COMMON/TAPE/IPROT
C
C
NAMELIST/RKTINP/EQL,FROZ,SUBAR,SUPAR,PCP
ITH = 0
210 DO 300 I=1,26
SUBAR(I) = 0.
300 CONTINUE
HPSP = .TRUE.
HP = .TRUE.
TPSP = .FALSE.

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D-77

LMSC/HREC D162424

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| FQL=.FALSE. | 380 |
| FROZ = .TRUE. | |
| IF(IPROT.EQ.1)T(1)=0. | 400 |
| IF (T(1).EQ.0.) GO TO 302 | 410 |
| TPSP = .TRUE. | 420 |
| TP = .TRUE. | 430 |
| HPSP = .FALSE. | 440 |
| GO TO 303 | 450 |
| 302 T(1) = 3800. | 460 |
| 303 IF(PCP(1).NE.0.) GO TO 308 | 470 |
| DO 305 I=1,NP | 480 |
| K = NP-I+2 | 490 |
| P(K) = P(K-1) | 500 |
| 305 CONTINUE | 510 |
| GO TO 311 | 520 |
| 308 NP= 2 | 530 |
| DO 310 I=1,24 | 540 |
| IF (I.GT.2) GO TO 309 | 550 |
| IF ((PCP(I).EQ.0.) .OR. PCP(I).EQ.1.) GO TO 310 | 560 |
| 309 IF (PCP(I).EQ.0.) GO TO 311 | 570 |
| NP = NP + 1 | 580 |
| P(NP) = P(1)/PCP(I) | 590 |
| 310 CONTINUE | 600 |
| 311 NSUB=0 | 610 |
| NSUP = 0 | 620 |
| DO 320 I=1,13 | 630 |
| IF(SUBAR(I).NE.0.)NSUB=NSUB+1 | 640 |
| IF(SUPAR(I).NE.0.)NSUP=NSUP+1 | 650 |
| 320 CONTINUE | |
| IF(IFLG1.EQ.0)GO TO 294 | 660 |
| WRITE (6,RKTINP) | |
| 294 CONTINUE | 680 |
| ITROT= 3 | 670 |
| SSO = 0. | 690 |
| TT = T(1) | 700 |
| C | 710 |
| C SET ASSIGNED P | 720 |
| C | |

| | | |
|------|--|------|
| | DO 902 IP = 1,NP | 730 |
| | PP = P(IP) | 740 |
| | CALL EQLBRM | 750 |
| C | | |
| | IF(IFLG1.EQ.0)GO TO 291 | |
| | WRITE(6,5200)TT,NPT | |
| 5200 | FORMAT(11HOTT IN RKT=E10.3,2X,4HNPT=15) | |
| 291 | CONTINUE | |
| C | | |
| | T(NPT) = TT | 760 |
| | IF(TT.NE.0.) GO TO 333 | 770 |
| | IF(NPT.EQ.0) GO TO 1000 | 780 |
| | GO TO 900 | 790 |
| 333 | PCP(NPT) = P(1)/PP | 800 |
| | IF(IP.GT.1) GO TO 195 | 810 |
| C | | 820 |
| C | COMBUSTION CHAMBER | 830 |
| C | | 840 |
| | TP = .FALSE. | 850 |
| | HP = .FALSE. | 860 |
| | SP = .TRUE. | 870 |
| | S0 = SSUM(1) | 880 |
| | PCP(2)=((GAMMAS(1)+1.)/2.)**(GAMMAS(1)/(GAMMAS(1)-1.)) | 890 |
| | P(2) = P(1)/PCP(2) | 900 |
| | TT = 2.*TT/(GAMMAS(1)+1.) | 910 |
| | GO TO 900 | 920 |
| 195 | IF(IP.GT.2) GO TO 900 | 930 |
| C | | 940 |
| C | THROAT | 950 |
| C | | 960 |
| 190 | IF(ITH.NE.2) GO TO 191 | 970 |
| | ITH = 0 | 980 |
| | GAMMAS(2) = 0. | 990 |
| | GO TO 900 | 1000 |
| 191 | DH = HSUM(1)-HSUM(2) | 1010 |
| | DHSTAR = DH-GAMMAS(2)*TT*ENN/2. | 1020 |
| | IF (IDEBUG) WRITE(6,923)DHSTAR,HSUM(1),HSUM(2),PCP(2) | 1030 |
| 923 | FORMAT(4E25.8) | 1040 |

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|---|---|------|
| | DH = DHSTAR/DH | 1050 |
| | IF(DH.LT.0.) DH=-DH | 1060 |
| | IF(DH.LE.0.4E-4.OR.ITROT.EQ.0) GO TO 900 | 1070 |
| | IF(JSOL.NE.0) ITH =1 | 1080 |
| | IF (JSOL.EQ.0.AND.ITH.EQ.1) ITH=2 | 1090 |
| | IF(ITH.EQ.0) GO TO 192 | 1100 |
| C | | 1110 |
| C | SPECIAL THROAT INTERPOLATION IF ITH = 2 | 1120 |
| C | | 1130 |
| | DLNI = .5*TT*ENN/(HSUM(1)-HSUM(2)) | 1140 |
| | AA(ITH)=.5*DLNI*(2.*DLNI+(GAMMAS(2)-1.)/GAMMAS(2)) | 1150 |
| | XX = ALOG(PCP(2)) | 1160 |
| | BB(ITH) = 1./GAMMAS(2)-DLNI-2.*XX*AA(ITH) | 1170 |
| | CC(ITH) = ENN*TT/(PP*(HSUM(1)-HSUM(2))**.5) | 1180 |
| | CC(ITH) = ALOG(CC(ITH))-XX*(BB(ITH)+AA(ITH)*XX) | 1190 |
| | IF(ITH.EQ.1) GO TO 192 | 1200 |
| | BB(1)=BB(1)-BB(2) | 1210 |
| | AA(1)=AA(1)-AA(2) | 1220 |
| | PCP(2)=(-BB(1)+(BB(1)*BB(1)-4.*AA(1)*(CC(1)-CC(2))**.5)/(2.*AA(1) | 1230 |
| | 1) | 1240 |
| | PCP(2)=EXP(PCP(2)) | 1250 |
| | GO TO 193 | 1260 |
| | 192 PCP(2)= PCP(2)/(1.+2.*DHSTAR/(ENN*TT *(GAMMAS(2)+1.))) | 1270 |
| | 193 P(2) = P(1) / PCP(2) | 1280 |
| | PP = P(2) | 1290 |
| | ITROT = ITROT-1 | 1300 |
| | CALL EQLBRM | 1310 |
| | IF(TT.EQ.0.) GO TO 1000 | 1320 |
| | GO TO 190 | 1330 |
| C | | 1340 |
| | 900 K = 0 | 1350 |
| | IF (.NOT.EQL .AND. FROZ) GO TO 990 | 1360 |
| | IF(IP.EQ.NP.OR.TT.EQ.0.) GO TO 860 | 1370 |
| | K = NPT | 1380 |
| | IF(NPT.NE.13) GO TO 870 | 1390 |
| | 860 CALL RKTOUT | 1400 |
| | IF(K.EQ.0) GO TO 990 | 1420 |
| | WRITE(6,865) | 1430 |

| | | |
|------|---|------|
| 865 | FORMAT(1H1) | 1440 |
| | NPT = 2 | 1450 |
| 870 | NPT = NPT + 1 | 1460 |
| C | | 1470 |
| C | SAVE COMPOSITIONS FOR ESTIMATES OF NEXT POINT | 1480 |
| C | | 1490 |
| | DO 880 I = 1,NS | 1500 |
| | EN(I,NPT) = EN(I,K) | 1510 |
| 880 | CONTINUE | 1520 |
| 902 | CONTINUE | 1530 |
| 990 | IF (FROZ) CALL FROZEN | 1540 |
| 1000 | RETURN | 1550 |
| | END | 1560 |

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$ORIGIN      E
$IBFTC CECS4  DECK
C                                                    10
      SUBROUTINE EQLBRM                                20
C  ROUTINE TO CALCULATE EQUILIBRIUM COMPOSITION AND PROPERTIES  30
C                                                    40
      DOUBLE PRECISION X,G                            50
      LOGICAL HP,SP,TP,IDEBUG,CONVG,IONS,MOLES,FROZ,EQL,LOGV,HPSP,TPSP  60
      LOGICAL ISING,IC                                70
C                                                    80
      DIMENSION PROW(18)                              90
C                                                    100
      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)  110
1     ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)  120
2     ,TOTN(13)                                       130
      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)  140
1     ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)      150
      COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)  160
1     ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)  170
2     ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)  180
3     ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)  190
4     ,RHOP,RMW(15),TLN                                       200
      COMMON /DOUBLE/ G(20,21), X(20)                 210
      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM  220
1     ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ  230
2     ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1           240
      COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)  250
1     ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SSO               260
C                                                    270
      COMMON/CASENO/LST
      EQUIVALENCE (NLM,L)                                280
C                                                    290
      DATA ITER/4HITER/,IE/1HE/,SMALNO/1.E-6/,SMNOL/-13.815511/  300
C                                                    310
      SIZE= 18.5                                          320
      ISING = .FALSE.                                     330
      ENNL = ALOG(ENN)                                    340
      LOGV = .FALSE.                                     350

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|--|-----|
| PPLN = ALOG(PP) | 360 |
| TLN = ALOG(TT) | 370 |
| CONVG = .FALSE. | 380 |
| ITNUMB = ITN | 390 |
| IF(IC) GO TO 966 | 400 |
| IF (.NOT.IONS.OR.IE.EQ.LLMT(L)) GO TO 33 | 410 |
| L = L+1 | 420 |
| IQ1 = IQ1+1 | 430 |
| DO 499 J = 1,NS | 440 |
| IF (A(L,J) .EQ.0.) GO TO 499 | 450 |
| EN(J,NPT) = SMALNO | 460 |
| ENLN(J) = SMNOL | 470 |
| IUSF(J) = 0 | 480 |
| 499 CONTINUE | 490 |
| 33 IF(NPT.EQ.1) WRITE(6,244)(LLMT(I),I=1,L),ITER | 500 |
| 244 FORMAT (4H0PT ,14(5X,A4)) | 510 |
| 43 TM = ALOG(PP/ENN) | 520 |
| JS1 = 1 | 530 |
| IF(.NOT.TP) CALL CPHS | 540 |
| IF(TP.AND.(CONVG.OR.ITNUMB.EQ.ITN)) CALL CPHS | 550 |
| IF(IC) GO TO 171 | 560 |
| IF (.NOT.CONVG.OR.JSOL.EQ.0) GO TO 62 | 570 |
| ENSOL = EN(JSOL,NPT) | 580 |
| EN(JSOL,NPT) = EN(JSOL,NPT)+EN(JLIQ,NPT) | 590 |
| IUSE(JLIQ) = -IUSE(JLIQ) | 600 |
| IQ1 = IQ1-1 | 610 |
| DLVTP(NPT) = 0. | 620 |
| CPR(NPT) = 0. | 630 |
| GAMMAS(NPT) = 0. | 640 |
| LOGV = .TRUE. | 650 |
| 62 CALL MATRIX | 660 |
| NUMB = ITN-ITNUMB+1 | 670 |
| IF(.NOT.CONVG) GO TO 67 | 680 |
| IF (LOGV.AND.JSOL.EQ.0) GO TO 63 | 690 |
| DO 182 I=1,L | 700 |
| PROW(I) = G(IQ1,I) | 710 |
| 182 CONTINUE | 720 |
| IF (.NOT.LOGV) GO TO 67 | 730 |

| | | |
|---|--|------|
| C | | 740 |
| C | LOGV = .TRUE.-- SET UP MATRIX TO SOLVE FOR DLVPT | 750 |
| C | | 760 |
| | 63 G(IQ1,IQ2) = ENN | 770 |
| | IQ = IQ1 - 1 | 780 |
| | DO 777 I = 1,IQ | 790 |
| | G(I,IQ2) = G(I,IQ1) | 800 |
| | 777 CONTINUE | 810 |
| | 67 IF (.NOT.IDEBUG) GO TO 72 | 820 |
| | WRITE(6,772) NUMB | 830 |
| | 772 FORMAT (11H01 ITERATION ,I3,6X,7HMATRIX //) | 840 |
| | DO 911 I=1,IMAT | 850 |
| | 911 WRITE (6,73) (G(I,K),K=1,KMAT) | 860 |
| | 72 IF(CONVG) IMAT=IMAT-1 | 870 |
| | ITST = IMAT | 880 |
| | CALL MGAUSD | 890 |
| | IF(ITST.NE.IMAT) GO TO 774 | 900 |
| | IF(.NOT.IDEBUG.OR.CONVG) GO TO 773 | 910 |
| | WRITE (6,373)(LLMT(I),I=1,L) | 920 |
| | 373 FORMAT (7H0PI ,9(A4,10X)) | 930 |
| | WRITE (6,73)(X(I),I=1,IMAT) | 940 |
| | 73 FORMAT (9E14.6) | 950 |
| | 773 IF(.NOT.CONVG) GO TO 85 | 960 |
| | IF(LOGV) GO TO 171 | 970 |
| | 174 SUM = 0. | 980 |
| | DO 175 J=1,L | 990 |
| | SUM = SUM+PROW(J)*X(J) | 1000 |
| | 175 CONTINUE | 1010 |
| | DLVTP(NPT) = 1.+G(IQ2,IQ1)/ENN-SUM/ENN - X(IQ1) | 1020 |
| | CPR(NPT) = G(IQ2,IQ2) | 1030 |
| | DO 176 J=1,IQ1 | 1040 |
| | CPR(NPT) = CPR(NPT)-G(IQ2,J)*X(J) | 1050 |
| | 176 CONTINUE | 1060 |
| | LOGV = .TRUE. | 1070 |
| | GO TO 62 | 1080 |
| C | | 1090 |
| C | SINGULAR MATRIX | 1100 |
| C | | 1110 |

| | | |
|-----|---|--------------|
| 774 | IF(.NOT.CONVG) GO TO 775 | 1120 |
| | WRITE(6,172) | 1130 |
| 172 | FORMAT(28H0DERIVATIVE MATRIX SINGULAR) | 1140 |
| | IC = .TRUE. | 1150 |
| | GO TO 171 | 1160 |
| 775 | IF (.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.) GO TO 871 | 1170 |
| | WRITE(6,874) | 1180 |
| 874 | FORMAT(96H0LOW TEMPERATURE IMPLIES CONDENSED SPECIES SHOULD HAVE 1BEEN INCLUDED ON AN INSERT CARD, RESTART) | 1190 1200 |
| | GO TO 873 | 1210 |
| 871 | WRITE (6,74) | 1220 |
| 74 | FORMAT(16H0SINGULAR MATRIX) | 1230 |
| | IF(IC) GO TO 873 | 1240 |
| | IF (ISING) GO TO 997 | 1250 |
| | NTZERO = 0 | 1260 |
| 966 | DO 970 JJ = 1, NS | 1270 |
| | IF(IUSE(JJ)) 970,968,967 | 1280 |
| 967 | IF(EN(JJ,NPT).EQ.0.) GO TO 873 | 1290 |
| | GO TO 969 | 1300 |
| 968 | IF(EN(JJ,NPT).NE.0.) GO TO 969 | 1310 |
| | EN(JJ,NPT) = SMALNO | 1320 |
| | ENLN(JJ) = SMNOL | 1330 |
| | GO TO 970 | 1340 |
| 969 | NTZERO = NTZERO+1 | 1350 |
| 970 | CONTINUE | 1360 |
| | IF(.NOT.IC) GO TO 971 | 1370 |
| | IC = .FALSE. | 1380 |
| | GO TO 43 | 1390 |
| 971 | ISING = .TRUE. | 1400 |
| | WRITE (6,776) | 1410 |
| 776 | FORMAT (8H0RESTART) | 1420 |
| | GO TO 43 | 1430 |
| 997 | IF(NTZERO.NE.(L-1)) GO TO 873 | 1440 |
| | IF(EQRAT.GT.1.00001.OR.EQRAT.LT.0.99999) GO TO 873 | 1450 |
| | ENN=0. | 1460 |
| | NEN = 0 | 1470 |
| | DO 83 I=1,L | 1480 |
| | JEN=0 | 1490 |

| | | |
|-----|---|------|
| | DO 80 J=1,NS | 1500 |
| | IF(EN(J,NPT).EQ.0.) GO TO 80 | 1510 |
| | IF(A(I,J).EQ.0.) GO TO 80 | 1520 |
| | IF(JEN.NE.0) GO TO 83 | 1530 |
| | JEN = J | 1540 |
| 80 | CONTINUE | 1550 |
| | NEN = NEN+1 | 1560 |
| | EN(JEN,NPT) = B0(I)/A(I,JEN) | 1570 |
| 83 | CONTINUE | 1580 |
| | IF(NEN.LT.NTZERO) GO TO 873 | 1590 |
| | CONVG = .TRUE. | 1600 |
| | IC = .TRUE. | 1610 |
| | HSUM(NPT) = 0. | 1620 |
| | DO 84 J=1,NS | 1630 |
| | IF(EN(J,NPT).EQ.0.) GO TO 84 | 1640 |
| | ENN = EN(J,NPT)+ENN | 1650 |
| | TEM = EN(J,NPT) | 1660 |
| | ENLN(J) = ALOG(TEM) | 1670 |
| | HSUM(NPT) = HSUM(NPT) + EN(J,NPT)*H0(J) | 1680 |
| 84 | CONTINUE | 1690 |
| | TM = ALOG(PP/ENN) | 1700 |
| | GO TO 43 | 1710 |
| 85 | ITNUMB= ITNUMB-1 | 1720 |
| | | 1730 |
| C | | 1740 |
| C | OBTAIN CORRECTIONS TO THE ESTIMATES | 1750 |
| | | 1760 |
| | KK = L + 1 | 1770 |
| | DLNT= X(IQ2) | 1780 |
| | IF (TP) DLNT=0. | 1790 |
| | DO 101 J=1,NS | 1800 |
| | IF (IUSE(J)) 101,98,100 | 1810 |
| 98 | DELN(J) = H0(J)*DLNT-H0(J)+S(J)-ENLN(J)-TM+X(IQ1) | 1820 |
| | DO 99 K=1,L | 1830 |
| | DELN(J)= DELN(J)+A(K,J)*X(K) | 1840 |
| 99 | CONTINUE | 1850 |
| | GO TO 101 | 1860 |
| 100 | DELN(J) = X(KK) | 1870 |
| | KK = KK + 1 | |

| | | |
|-----|--|------|
| 101 | CONTINUE | 1880 |
| | AMBDA= 1. | 1890 |
| | AMBDA1= 1. | 1900 |
| | SUM = X(IQ1) | 1910 |
| | IF(SUM.LT.0.) SUM=-SUM | 1920 |
| | IF(DLNT.GT.SUM) SUM=DLNT | 1930 |
| | IF(-DLNT.GT.SUM) SUM=-DLNT | 1940 |
| | DO 917 J=1,NS | 1950 |
| | IF (IUSE(J).NE.0) GO TO 917 | 1960 |
| | IF((EN(J,NPT).GT.0.).AND.DELN(J).GT.SUM) SUM = DELN(J) | 1970 |
| | IF((EN(J,NPT).NE.0.) .OR. DELN(J).LE.0.) GO TO 917 | 1980 |
| | SUM1 = (-9.212-ENLN(J)+ENNL)/(DELN(J)-X(IQ1)) | 1990 |
| | IF(SUM1.LT.0.) SUM1=-SUM1 | 2000 |
| | IF (SUM1.LT.AMBDA1) AMBDA1 = SUM1 | 2010 |
| 917 | CONTINUE | 2020 |
| | IF(SUM.GT.2.)AMBDA=2./SUM | 2030 |
| | IF (AMBDA1.LT.AMBDA) AMBDA = AMBDA1 | 2040 |
| | IF (.NOT.IDEBUG) GO TO 111 | 2050 |
| | WRITE(6,923) TT,ENN,ENNL,PP,PPLN,AMBDA | 2060 |
| 923 | FORMAT (3H0T=,E15.8,6H ENN=,E15.8,7H ENNL=E15.8,5H PP=,E15.8, | 2070 |
| | 1 7H PPLN=E15.8,8H AMBDA=E15.8) | 2080 |
| | WRITE (6,924) | 2090 |
| 924 | FORMAT(1H0,18X,2HNI,12X,5HLN NI,8X,9HDEL LN NI,10X,4HH/RT,9X,4HS0/ | 2100 |
| | 1R,12X,6H-G0/RT,9X,5H-G/RT) | 2110 |
| | DO 926 J=1,NS | 2120 |
| | FNEG1 = S(J)-H0(J) | 2130 |
| | FNEG2 = FNEG1 | 2140 |
| | IF(IUSE(J).EQ.0) FNEG2=FNEG2-ENLN(J)-TM | 2150 |
| | WRITE (6,925) SUB(J,1),SUB(J,2), | 2160 |
| | 1SUB(J,3),EN(J,NPT),ENLN(J),DELN(J),H0(J),S(J),FNEG1,FNEG2 | 2170 |
| 925 | FORMAT (1X,3A4,7E15.6) | 2180 |
| 926 | CONTINUE | 2190 |
| | WRITE (6,110) | 2200 |
| 110 | FORMAT(1H0) | 2210 |
| C | | 2220 |
| C | APPLY CORRECTIONS TO ESTIMATES | 2230 |
| C | | 2240 |
| 111 | SUM = 0. | 2250 |

| | | |
|------|---|------|
| | DO 113 J=1,NS | 2260 |
| | IF (IUSE(J)) 113,112,114 | 2270 |
| 112 | ENLN(J)=ENLN(J)+AMBDA*DELN(J) | 2280 |
| | EN(J,NPT) = 0. | 2290 |
| | IF((ENLN(J)-ENNL+SIZE).LE.0.) GO TO 113 | 2300 |
| | EN(J,NPT) = EXP(ENLN(J)) | 2310 |
| | SUM = SUM+EN(J,NPT) | 2320 |
| | GO TO 113 | 2330 |
| 114 | EN(J,NPT) = EN(J,NPT) + AMBDA * DELN(J) | 2340 |
| 113 | CONTINUE | 2350 |
| | SUMN = SUM | 2360 |
| | IF (TP) GO TO 115 | 2370 |
| | TLN= TLN+AMBDA*DLNT | 2380 |
| | TT = EXP(TLN) | 2390 |
| 115 | ENNL = ENNL+AMBDA*X(IQ1) | 2400 |
| | ENN = EXP(ENNL) | 2410 |
| | IF (LLMT(L).NE.1E) GO TO 116 | 2420 |
| C | | 2430 |
| C | CHECK ON REMOVING IONS | 2440 |
| C | | 2450 |
| | DO 1116 J = 1,NS | 2460 |
| | IF (A(L,J).EQ.0.) GO TO 1116 | 2470 |
| | IF (EN(J,NPT).GT.0.) GO TO 116 | 2480 |
| 1116 | CONTINUE | 2490 |
| | DO 1118 J=1,NS | 2500 |
| | IF(A(L,J).NE.0.) IUSE(J) = -10000 | 2510 |
| 1118 | CONTINUE | 2520 |
| | L = L-1 | 2530 |
| | IQ1 = IQ1-1 | 2540 |
| | GO TO 43 | 2550 |
| C | | 2560 |
| C | TEST FOR CONVERGENCE | 2570 |
| C | | 2580 |
| 116 | IF (ITNUMB.EQ.0) GO TO 13 | 2590 |
| | IF (AMBDA.LT.1.) GO TO 43 | 2600 |
| | SUM = (ENN-SUMN)/ENN | 2610 |
| | IF (SUM.LT.0.) SUM = -SUM | 2620 |
| | IF (SUM.GT.0.5E-5) GO TO 43 | 2630 |

| | |
|--|------|
| DO 130 J=1,NS | 2640 |
| IF (IUSE(J).LT.0) GO TO 130 | 2650 |
| AA= DELN(J)/SUMN | 2660 |
| IF(AA.LT.0.) AA=-AA | 2670 |
| IF (IUSE(J).EQ.0) AA = AA*EN(J,NPT) | 2680 |
| 129 IF(AA.GT.0.5E-5) GO TO 43 | 2690 |
| 130 CONTINUE | 2700 |
| 13 CONV= .TRUE. | 2710 |
| IF(TT .LT.TLOW.OR.TT .GT.THIGH)WRITE (6,306)TT ,NPT | 2720 |
| 306 FORMAT(17H0THE TEMPERATURE=E12.4,26H IS OUT OF RANGE FOR POINT,15) | 2730 |
| IF(ITNUMB.NE.0, GO TO 160 | 2740 |
| WRITE(6,973) ITN,NPT | 2750 |
| 973 FORMAT(1HL,I2.69H ITERATIONS DID NOT SATISFY CONVERGENCE REQUIREME | 2760 |
| INTS FOR THE POINT 15) | 2770 |
| IF (.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.OR.TT.GT.100.) GO TO 873 | 2780 |
| WRITE(6,874) | 2790 |
| TT = T(1) | 2800 |
| RETURN | 2810 |
| C | 2820 |
| C CONVERGENCE TESTS ARE SATISFIED, TEST CONDENSED SPECIES. | 2830 |
| C | 2840 |
| 160 IF(NC.EQ.0) GO TO 143 | 2850 |
| SIZEF = 0. | 2860 |
| INC = 0 | 2870 |
| DO 170 J = 1,NS | 2880 |
| IF (IUSE(J).EQ.0 .OR. IUSE(J).EQ.-10000) GO TO 170 | 2890 |
| INC = INC + 1 | 2900 |
| IF(IDEBUG) WRITE(6,144)(SUB(J,I),I=1,3),TEMP(INC,1),TEMP(INC,2), | 2910 |
| 1 IUSE(J),EN(J,NPT) | 2920 |
| 144 FORMAT (1H0,3A4,2F10.3,3X,5HIUSE=,I4,E15.7) | 2930 |
| IF (EN(J,NPT)) 146,148,169 | 2940 |
| 146 IF (J.NE.JSOL .AND. J .NE.JLIQ) GO TO 147 | 2950 |
| JSOL = 0 | 2960 |
| JLIQ = 0 | 2970 |
| 147 IQ1 = IQ1 - 1 | 2980 |
| EN(J,NPT) = 0. | 2990 |
| GO TO 166 | 3000 |
| 148 KG = 1 | 3010 |

| | | |
|-----|---|------|
| | IF(IUSE(J).EQ.-IUSE(J+1)) GO TO 154 | 3020 |
| 151 | IF(J.EQ.1.OR.IUSE(J).NE.-IUSE(J-1)) GO TO 153 | 3030 |
| | KG = -1 | 3040 |
| 154 | JKG = J + KG | 3050 |
| | IF (EN(JKG,NPT).LT.0.) GO TO 170 | 3060 |
| | TMELT = TEMP(INC,1) | 3070 |
| | IMP = INC + KG | 3080 |
| | IF(TMELT.EQ.TEMP(IMP,2)) GO TO 158 | 3090 |
| | TMELT = TEMP(INC,2) | 3100 |
| | IF (TMELT.EQ.TEMP(IMP,1)) GO TO 157 | 3110 |
| | WRITE (6,156) | 3120 |
| 156 | FORMAT (50H03 PHASES OF A CONDENSED SPECIES ARE OUT OF ORDER | 3130 |
| C | | 3140 |
| C | JTH SPECIES A SOLID (EN=0), (J+KG)TH SPECIES A LIQUID (EN IS +) | 3150 |
| C | | 3160 |
| 157 | IF(TT.GT.TMELT) GO TO 169 | 3170 |
| | IF (TP.AND.TT.EQ.TMELT) GO TO 169 | 3180 |
| | IF (TP) GO TO 1165 | 3190 |
| | IF (TT.LE.TMELT-150.) GO TO 1165 | 3200 |
| | JSOL = J | 3210 |
| | JLIQ = JKG | 3220 |
| | GO TO 159 | 3230 |
| C | | 3240 |
| C | JTH SPECIES A LIQUID(EN=0), (J+KG)TH SPECIES A SOLID (EN IS +) | 3250 |
| C | | 3260 |
| 158 | IF (TT.LT.TMELT) GO TO 169 | 3270 |
| | IF (TP.AND.TT.EQ.TMELT) GO TO 169 | 3280 |
| | IF (TP) GO TO 1165 | 3290 |
| | IF (TT.GE.TMELT+150.) GO TO 1165 | 3300 |
| | JSOL = JKG | 3310 |
| | JLIQ = J | 3320 |
| 159 | TLN = ALOG (TMELT) | 3330 |
| | TT = TMELT | 3340 |
| | EN(JKG,NPT) = .5 * EN(JKG,NPT) | 3350 |
| | EN(J,NPT) = EN(JKG,NPT) | 3360 |
| | GO TO 165 | 3370 |
| C | | 3380 |
| C | WRONG PHASE INCLUDED FOR T INTERVAL. SWITCH EN | 3390 |

| | | |
|---|--|------|
| C | | 3400 |
| | 1165 EN(J,NPT) = EN (JKG, NPT) | 3410 |
| | IUSE(J) = -IUSE(J) | 3420 |
| | IUSE (JKG) = -IUSE(JKG) | 3430 |
| | EN(JKG,NPT)= 0. | 3440 |
| | GO TO 40 | 3450 |
| | 153 IF (TT.LT.TEMP(INC,1) .AND.TEMP(INC,1).NE.TLOW) GO TO 169 | 3460 |
| | IF (TT.GT.TEMP(INC,2)) GO TO 169 | 3470 |
| C | | 3480 |
| C | | 3490 |
| | SUM = 0. | 3500 |
| | DO 167 I = 1,L | 3510 |
| | SUM = SUM + A(I,J)*X(I) | 3520 |
| | 167 CONTINUE | 3530 |
| | DELF = H0(J)-S(J)-SUM | 3540 |
| | IF(IDEBUG) WRITE(6,168)DELF,SIZEF | 3550 |
| | 168 FORMAT (17H GO-SUM(AIJ*PI) =E15.7,10X,18HPREVIOUS DELTA G =,E15.7) | 3560 |
| | IF(DELF.GE.SIZEF .OR. DELF.GE.0.) GO TO 169 | 3570 |
| | SIZEF = DELF | 3580 |
| | JDELF = J | 3590 |
| | 169 IF(INC.EQ.NC) GO TO 1160 | 3600 |
| | 170 CONTINUE | 3610 |
| | 1160 IF (SIZEF.EQ.0.) GO TO 143 | 3620 |
| | J = JDELF | 3630 |
| | 165 IQ1 = IQ1 + 1 | 3640 |
| | 166 IUSE(J) = - IUSE(J) | 3650 |
| | 40 CONVG = .FALSE. | 3660 |
| | 143 TN = NUMB | 3670 |
| | WRITE(6,771)NPT,(X(IL),IL=1,L),TN | 3680 |
| | 771 FORMAT (I3,14F9.3) | 3690 |
| | ITNUMB = ITN | 3700 |
| | GO TO 43 | 3710 |
| | | 3720 |
| C | | 3730 |
| C | CALCULATE EQUILIBRIUM PROPERTIES | 3740 |
| C | | 3750 |
| | 171 SSUM(NPT) = 0. | 3760 |
| | IF(JLIQ.NE.0) EN(JSOL,NPT)=ENSOL | 3770 |
| | DO 183 J=1,NS | |

| | | |
|------|---|------|
| | IF (NPT.EQ.1) SS0 = SS0 + EN(J,1)*S(J) | 3780 |
| | WRITE(6,7689)SS0,EN(J,1),S(J) | |
| 7689 | FORMAT(1H0,4HSS0=E10.3,2X,3HEN=E10.3,2X,2HS=E10.3) | |
| | SS = S(J) | 3790 |
| | IF(IUSE(J).EQ.0) SS=SS-ENLN(J)-TM | 3800 |
| | SSUM(NPT) = SSUM(NPT)+SS*EN(J,NPT) | 3810 |
| 183 | CONTINUE | 3820 |
| | IF(.NOT.IC) GO TO 178 | 3830 |
| | DLVPT(NPT) = -1. | 3840 |
| | DLVTP(NPT) = 1. | 3850 |
| | CPR(NPT) = CPSUM | 3860 |
| | GO TO 199 | 3870 |
| 178 | SUM = 0. | 3880 |
| | DO 179 J = 1,L | 3890 |
| | SUM = SUM + PROW(J)*X(J) | 3900 |
| 179 | CONTINUE | 3910 |
| | DLVPT(NPT) = -2.+SUM/ENN+ X(IQ1) | 3920 |
| 184 | IF(JLIQ.EQ.0) GO TO 199 | 3930 |
| | IUSE(JLIQ) = -IUSE(JLIQ) | 3940 |
| | HSUM(NPT) = HSUM(NPT)+EN(JLIQ,NPT)*(H0(JLIQ)-H0(JSOL)) | 3950 |
| | IQ1 = IQ1+1 | 3960 |
| | GAMMAS(NPT) = -1./DLVPT(NPT) | 3970 |
| | GO TO 186 | 3980 |
| 199 | GAMMAS(NPT) = -1./((DLVPT(NPT)+(DLVTP(NPT)**2)*ENN/CPR(NPT)) | 3990 |
| 186 | TTT(NPT) = TT | 4000 |
| | PPP(NPT) = PP | 4010 |
| | CPRF(NPT) = CPSUM | 4020 |
| | HSUM(NPT) = HSUM(NPT)*TT | 4030 |
| | WM(NPT) = 1./ENN | 4040 |
| 200 | IF (.NOT.IDEBUG) RETURN | 4050 |
| | WRITE(6,201) NPT,PCP(NPT),PP,TT,HSUM(NPT),SSUM(NPT),WM(NPT),CPR(NP | 4060 |
| | I T),DLVPT(NPT),DLVTP(NPT),GAMMAS(NPT) | 4070 |
| 201 | FORMAT (7H0POINT=13.3X,4HPCP=E13.6,3X,2HP=E13.6,3X,2HT=E13.6,3X,4H | 4080 |
| | 1H/R=E13.6,3X,4HS/R=E13.6//3X,3HMW=E13.6,3X,5HCP/R=E13.6,3X,6HDLVPT | 4090 |
| | 2=E13.6,3X,6HDLVTP=E13.6,3X,9HGAMMA(S)=E13.6) | 4100 |
| | GO TO 1000 | 4110 |
| C | | 4120 |
| C | ERROR, SET TT=0 | 4130 |

C
873 TT=0.
NPT = NPT-1
1000 RETURN
END

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$IBFTC CECS17 DECK
C
SUBROUTINE FROZEN
C
(FROZEN COMPOSITION EXPANSION ONLY)
C
LOGICAL EQL,FROZ,CONVG
C
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2 ,TOTN(13)
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2)
1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4 ,RHOP,RMW(15),TLN
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1 ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SSO
COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1 ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMTI9,FA1,FA2
2 ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FRI(2)
ITROT = 3
EQL = .FALSE.
NPT = 2
TT = TTT(1)
TLN=ALOG(TT)
WRITE(6,9009)TT,SS0,CPRF(1),PCP(1),WM(1),TLN,GAMMAS(1)
9009 FORMAT(1H0,3HTT=E10.3,4HSS0=E10.3,5HCPRF=E10.3,4HPCP=E10.3,
13HWM=E10.3,4HTLN=E10.3,7HGAMMAS=E10.3)
GAMMAS(1) = CPRF(1)/(CPRF(1)-1./WM(1))
CPR(1) = CPRF(1)
PCP(2) = ((GAMMAS(1)+1.)/2.)*(GAMMAS(1)/(GAMMAS(1)-1.))
DATA(1) = 2./(GAMMAS(1) + 1.)

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D-94

LMSC/HIREC D162424

| | | |
|----|---------------------------------------|-----|
| | TLN = TLN + ALOG(DATA(1)) | 350 |
| | DO 902 IP=2,NP | 360 |
| | IF(NPT.EQ.2) GO TO 45 | 370 |
| | PCP(NPT) = P(1)/P(IP) | 380 |
| 45 | CONVG = .FALSE. | 390 |
| | PCPLN= ALOG(PCP(NPT)) | 400 |
| | S0 = SS0 -PCPLN/WM(1) | 410 |
| | SUMH = 0. | 420 |
| 51 | TT=EXP(TLN) | 430 |
| | SUMS=0. | 440 |
| | JS1 = 1 | 450 |
| | NNN = NPT | 460 |
| | NPT = 1 | 470 |
| | CALL CPHS | 480 |
| | NPT = NNN | 490 |
| | DO 60 J=1,NS | 500 |
| | IF(EN(J,1).EQ.0.) GO TO 60 | 510 |
| | SUMS = SUMS + S(J)*EN(J,1) | 520 |
| | IF(CONVG) SUMH=SUMH+H0(J)*EN(J,1) | 530 |
| 60 | CONTINUE | 540 |
| | IF (CONVG) GO TO 81 | 550 |
| | DLNT=(SUMS-S0)/CPSUM | 560 |
| | TLN=TLN-DLNT | 570 |
| | IF(DLNT.LT.0.) DLNT=-DLNT | 580 |
| | IF(DLNT.LT.0.5E-4) CONVG=.TRUE. | 590 |
| | GO TO 51 | 600 |
| 81 | TTT(NPT)= TT | 610 |
| | SSUM(NPT)= SSUM(1) | 620 |
| | HSUM(NPT)= TT*SUMH | 630 |
| | GAMMAS(NPT)= CPSUM/(CPSUM-1./WM(1)) | 640 |
| | IF(IP.GT.2) GO TO 90 | 650 |
| C | | 660 |
| C | THROAT CALCULATIONS | 670 |
| C | | 680 |
| | DH = HSUM(1)-HSUM(2) | 690 |
| | DHSTAR = DH-(GAMMAS(2)*TT/(2.*WM(1))) | 700 |
| | DH = DHSTAR/DH | 710 |
| | IF(DH.LT.0.) DH=-DH | 720 |

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| IF(DH.LE.0.4E-4.OR.ITROT.EQ.0) GO TO 90 | 730 |
| PCP(2) = PCP(2)/(1.+2.*DHSTAR*WM(1)/(TT*(GAMMAS(2)+1.))) | 740 |
| P(2) = P(1)/PCP(2) | 750 |
| ITROT = ITROT-1 | 760 |
| GO TO 45 | 770 |
| 90 WM(NPT)= WM(1) | 780 |
| PPP(NPT) = P(IP) | 790 |
| CPR(NPT)= CPSUM | 800 |
| K = 0 | 810 |
| IF (TT.LT.(TLOW-150.))GO TO 903 | 820 |
| IF(NC.EQ.0) GO TO 700 | 830 |
| INC = 0 | 840 |
| DO 901 I=1,NS | 850 |
| IF(IUSE(I).EQ.0.OR.IUSE(I).EQ.-10000) GO TO 901 | 860 |
| INC = INC+1 | 870 |
| IF(EN(I,1).EQ.0.) GO TO 901 | 880 |
| IF (TT.LT.(TEMP(INC,1)-50.).OR.TT.GT.(TEMP(INC,2)+50.))GO TO 903 | 890 |
| 901 CONTINUE | 900 |
| 700 IF (IP.EQ.NP) GO TO 863 | 910 |
| K = NPT | 920 |
| IF (NPT.NE.13) GO TO 870 | 930 |
| GO TO 863 | 940 |
| 903 NPT = NPT - 1 | 950 |
| 863 CALL RKTOUT | 960 |
| GO TO 1000 | |
| 865 IF (K.EQ.0) GO TO 1000 | 980 |
| NPT = 2 | 990 |
| 870 NPT = NPT + 1 | 1000 |
| 902 CONTINUE | 1010 |
| 1000 RETURN | 1020 |
| END | 1030 |

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$IBFTC CECS9  DECK
C
SUBROUTINE HCALC
C
C CALCULATE ENTHALPY FOR PROPELLANT USING COEFFICIENTS
C
LOGICAL MOLES
DIMENSION NUM(15,5),WS(2)
C
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
C
EQUIVALENCE (ANUM,NUM),(L,NLM),(J,JS1)
C
DATA AG/1HG/,IZERO/2H00/,OX/1HO/
C
C IS TT IN RANGE
C
IF(TT.LT.(TLOW-100.).OR.TT.GT.(THIGH+1000.))GO TO 75
WS(1) = 0.
WS(2) = 0.
HPP(1)=0.
HPP(2)=0.
AC(1)=0.
AC(2)=0.
DO 900 N=1,NREAC
K=2
IF(FOX(N).EQ.OX)K=1
PCWT=PECWT(N)
IF(MOLES)PCWT=PCWT*RMW(N)

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| WS(K) = WS(K) + PCWT | 380 |
| IF(NAME(N,5).NE.IZERO)GO TO 500 | 390 |
| J = NUM(N,5) | 400 |
| IF (J.NE.0) GO TO 90 | 410 |
| DO 10 J=1,L | 420 |
| DATA(J)=0. | 430 |
| 10 CONTINUE | 440 |
| DO 40 I=1,4 | 450 |
| IF(ANUM(N,I).EQ.0.)GO TO 50 | 460 |
| DO 20 J=1,L | 470 |
| IF(LLMT(J).EQ.NAME(N,I)) GO TO 30 | 480 |
| 20 CONTINUE | 490 |
| 30 DATA(J)=ANUM(N,I) | 500 |
| 40 CONTINUE | 510 |
| 50 IS=0 | 520 |
| DO 70 J=1,NS | 530 |
| IF(IUSE(J).EQ.0)GO TO 55 | 540 |
| IS = IS+1 | 550 |
| IF(FAZ(N).EQ.AG)GO TO 70 | 560 |
| IF(TT.GT.TEMP(IS,2).AND.TEMP(IS,2).NE.THIGH) GO TO 70 | 570 |
| IF(TT.LT.TEMP(IS,1).AND.TEMP(IS,1).NE.TLOW) GO TO 70 | 580 |
| GO TO 56 | 590 |
| 55 IF(FAZ(N).NE.AG) GO TO 70 | 600 |
| 56 DO 60 I=1,L | 610 |
| IF(A(I,J).NE.DATA(I)) GO TO 70 | 620 |
| 60 CONTINUE | 630 |
| NUM(N,5) = J | 640 |
| GO TO 90 | 650 |
| 70 CONTINUE | 660 |
| DELN(J)= EN(J,NPT) | 700 |
| EN(J,NPT) = 1. | 710 |
| CALL CPHS | 720 |
| EN(J,NPT) = DELN(J) | 730 |
| NS = NSS | 740 |
| IF (H0(J).GT.-.01 .AND. H0(J).LT..01) H0(J) = 0. | 750 |
| RTEMP(N) = TT | 760 |
| ENTH(N) = H0(J)*R*TT | 770 |
| AC(K)=AC(K)+CPSUM*PCWT/RMW(N) | 780 |

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| 500 | HPP(K)=HF P(K)+ENTH(N)*PCWT/RMW(N) | 790 |
| 900 | CONTINUE | 800 |
| | DO 950 K=1,2 | 810 |
| | IF(WS(K).EQ.0.)GO TO 950 | 820 |
| | HPP(K)=HPP(K)/WS(K) | 830 |
| | AC(K)=AC(K)/WS(K) | 840 |
| | GO TO 80 | 670 |
| 90 | NSS = NS | 680 |
| | NS = J | 690 |
| 950 | CONTINUE | 850 |
| | HSUB0 = (WP(1)*HPP(1)+WP(2)*HPP(2))/(WP(1)+WP(2)) | 860 |
| | GO TO 1000 | 870 |
| 75 | WRITE(6,76) | 880 |
| 76 | FORMAT(50H0REACTANT TEMPERATURE OUT OF RANGE OF THERMO DATA) | 890 |
| 80 | WRITE(6,85) N | 900 |
| 85 | FORMAT(1H0,I2,34H TH REACTANT IS NOT IN THERMO DATA) | 910 |
| 1000 | RETURN | 920 |
| | END | 930 |

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| \$IBFTC CECS14 DECK | 10 |
| C | 20 |
| C ROCKET PERFORMANCE PERAMETERS | 30 |
| C | 40 |
| SUBROUTINE RKTOUT | 50 |
| C | 60 |
| LOGICAL EQL,FROZ ,TP,HP,SP,HPSP,TPSP,SHOCK | 70 |
| C | 80 |
| DIMENSION NV(13),Z(10,4),RHOISP(13) | 90 |
| C | 100 |
| COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13) | 110 |
| 1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13) | 120 |
| 2 ,TOTN(13) | 130 |
| COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150) | 140 |
| 1 ,DELN(150),A(15,150),SUB(150,3),9USE(150),TEMP(50,2) | 150 |
| COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2) | 160 |
| 1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2) | 170 |
| 2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5) | 180 |
| 3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15) | 190 |
| 4 ,RHOP,RMW(15),TLN | 200 |
| COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM | 210 |
| 1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWNR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ | 220 |
| 2 ,IONS,NC,NSERT,JSOL,JL IQ,KASE,NREAC,IC,JS1 | 230 |
| COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13) | 240 |
| 1 ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0 | 250 |
| COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4) | 260 |
| 1 ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2 | 270 |
| 2 ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FR1(2) | |
| COMMON/GASES/TAB(3,12,13),NMIX | |
| COMMON/SUNUP/SUN(3,40,2) | |
| COMMON/CASENO/LST | |
| COMMON/TAPE/IPROT | |
| COMMON/MOLFRC/ZFRAC(40),KF | 280 |
| C | 290 |
| EQUIVALENCE (V,NV),(Z,H0) | 300 |
| C | 310 |
| DATA EXIT/4HEXIT/ | 320 |
| C | |


```

LSP=LST
IF(EQL) WRITE (6,37) 330
37 FORMAT(1H1/24X,84HTHEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBR 340
IUM COMPOSITION DURING EXPANSION //) 350
IF (.NOT.EQL) WRITE (6,38) 360
38 FORMAT(1H1,26X,78HTHEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN C 370
OMPOSITION DURING EXPANSION //) 380
IF (TPSP) WRITE (6,737) 390
737 FORMAT (52X,28HAT AN ASSIGNED TEMPERATURE 400
V(1) = PPP(1)*14.696006 410
WRITE (6,40) V(1) 420
40 FORMAT(5H PC = ,F8.1,5H PSIA) 430
CALL OUT1 440
NEX = NPT - 2 450
DO 862 I = 1,NEX 460
862 V(I) = EXIT 470
WRITE(6,48) (V(I),I=1,NEX) 480
48 FORMAT(1H0,16X,16HCHAMBER THROAT ,11(5X,A4)) 490
C 500
C PRESSURE RATIOS 510
C 520
DO 45 I=1,NPT 530
K= 2*I+3 540
FMT(K)= F3 550
IF (PCP(I).GE.1000.) FMT(K)=F2 560
IF (PCP(I).GE.10000.)FMT(K)=F1 570
IF (PCP(I).GE.1000000.)FMT(K) = F0 580
45 CONTINUE 590
WRITE (6,FMT) FR1,FB,FB,FB,(PCP(J),J=1,NPT) 600
CALL OUT2 610
C 620
AGV = 9.80665 630
DO 202 K=2,NPT 640
SPIM(K) = (2.*RR*(HSUM(1)-HSUM(K)))*.5/AGV 650
C 660
C AW (A/W) IN UNITS OF SEC/ATM 670
C 680
AW = RR*TTT(K)/(PPP(K)* WM(K)*SPIM(K)*AGV**2) 690

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| | | |
|-----|--|------|
| | IF(K.NE.2)GO TO 200 | 700 |
| | AWT=AW | 710 |
| | CSTR=32.174*P(1)*AWT | 720 |
| 200 | AEAT(K)=AW/AWT | 730 |
| | VACI(K)=SPIM(K)+PPP(K)*AW | 740 |
| | IF (SONVEL(K).NE.0.) VMOC(K)=SPIM(K)*AGV/SONVEL(K) | 750 |
| | NV(K)= CSTR + .5 | 760 |
| 202 | CONTINUE | 770 |
| C | | 780 |
| C | MACH NUMBER | 790 |
| C | | 800 |
| | VMOC(1)=0. | 810 |
| | IF(GAMMAS(2).EQ.0.) VMOC(2)=0. | 820 |
| | FMT(7) = F3 | 830 |
| | WRITE(6,FMT)(FN(1),I=1,4),(VMOC(J),J=1,NPT) | 840 |
| | DO 520 JAB=1,NPT | |
| 520 | TAB(LSP,4,JAB)=VMOC(JAB) | |
| | WRITE (6,208) | 850 |
| 208 | FORMAT (1H) | 860 |
| C | | 870 |
| C | C* | 880 |
| C | | 890 |
| | FMT(4) = FMT9X | 900 |
| | FMT(5) = FMT13 | 910 |
| | FMT(6) = FMT19 | 920 |
| | FMT(7) = FB | 930 |
| | WRITE(6,FMT)(FR(1),I=1,4),(NV(J),J=2,NPT) | 940 |
| C | | 950 |
| C | CF - THRUST COEFICIENT | 960 |
| C | | 970 |
| | FMT(6) = FMT(8) | 980 |
| | FMT(7) = F3 | 990 |
| | DO 212 I=2,NPT | 1000 |
| 212 | V(I)=32.174*SPIM(I)/CSTR | 1010 |
| | WRITE(6,FMT)FC1,FB,FB,FB,(V(J),J=2,NPT) | 1020 |
| C | | 1030 |
| C | AREA RATIO | 1040 |
| C | | 1050 |

| | | |
|-----|--|------|
| | FMT(5) = FB | 1060 |
| | DO 214 I = 2,NPT | 1070 |
| | K = 2*I+3 | 1080 |
| | FMT(K) = F4 | 1090 |
| | IF (AEAT(I).GE.1.) FMT(K) = F3 | 1100 |
| | IF (AEAT(I).GE.10.) FMT(K) = F2 | 1110 |
| | IF (AEAT(I).GE.100.) FMT(K) = F1 | 1120 |
| 214 | CONTINUE | 1130 |
| | WRITE(6,FMT)FA1,FA2,FB,FB,(AEAT(J),J=2,NPT) | 1140 |
| | DO 530 JAB=1,NPT | |
| 530 | TAB(LSP,2,JAB)=AEAT(JAB) | |
| C | | 1150 |
| C | VACUUM IMPULSE | 1160 |
| C | | 1170 |
| | FMT(5) = FMT13 | 1180 |
| | FMT(7) = F1 | 1190 |
| | WRITE(6,FMT)(FA(I),I=1,4),(VACI(J),J=2,NPT) | 1200 |
| C | | 1210 |
| C | SPECIFIC IMPULSE | 1220 |
| C | | 1230 |
| | WRITE(6,FMT)(FI(I),I=1,4),(SPIM(J),J=2,NPT) | 1240 |
| | DO 308 J = 2,NPT | 1250 |
| 308 | RHOISP(J) = SPIM(J) * RHOP | 1260 |
| | WRITE (6,FMT) (FRI(I),I=1,2),FB,FB,(RHOISP(J),J=2,NPT) | 1270 |
| | WRITE (6,208) | 1280 |
| | FMT(4) = FB | 1290 |
| | FMT(5) = FMT13 | 1300 |
| | FMT(7) = F5 | 1310 |
| | IF(EQL) GO TO 312 | 1320 |
| | WRITE(6,310) | 1330 |
| 310 | FORMAT(15H0MOLE FRACTIONS //) | 1340 |
| C | | 1350 |
| C | MOLE FRACTIONS - FROZEN | 1360 |
| C | | 1370 |
| | LINE = 0 | 1380 |
| | KF=0 | |
| | DO 430 K =1,NS | 1390 |
| | V(LINE+1) = EN(K,1)/TOTN(1) | 1400 |

| | |
|---|------|
| IF (V(LINE+1).LT.(5.E-6)) GO TO 424 | 1410 |
| LINE = LINE+1 | 1420 |
| Z(LINE,1) = SUB(K,1) | 1430 |
| Z(LINE,2) = SUB(K,2) | 1440 |
| Z(LINE,3) = SUB(K,3) | 1450 |
| Z(LINE,4) = V(LINE) | 1460 |
| IF(V(LINE).LE..05) GO TO 561 | |
| KF=KF+1 | |
| ZFRAC(KF)=V(LINE) | |
| DO 560 JAB=1,NPT | |
| 560 TAB(LSP,KF+8,JAB)=V(LINE) | |
| SUN(LSP,KF,1)=SUB(K,1) | |
| SUN(LSP,KF,2)=SUB(K,2) | |
| WRITE(6,562)KF,SUN(LSP,KF,1),SUN(LSP,KF,2),SUB(K,1),SUB(K,2), | |
| \$ZFRAC(KF),V(LINE) | |
| 562 FORMAT(1H0,I5,5X,2A6,5X,2A6,5X,E10.3,5X,E10.3) | |
| 561 CONTINUE | |
| 424 IF (LINE.NE.4.AND.K.NE.NS) GO TO 430 | 1470 |
| IF (LINE.EQ.0) GO TO 312 | 1480 |
| WRITE (6,426) (Z(LN,1),Z(LN,2),Z(LN,3),Z(LN,4),LN=1,LINE) | 1490 |
| 426 FORMAT (1H ,4(3A4,F9.5,7X)) | 1500 |
| LINE = 0 | 1510 |
| 430 CONTINUE | 1520 |
| 312 CALL OUT3 | 1530 |
| 1000 RETURN | 1540 |
| END | 1550 |

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$IBFTC CECS19 DECK
  BLOCK DATA
  COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
  1  ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
  2  ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FR1(2)
C
C  INFORMATION USED IN VARIABLE OUTPUT FORMAT
C
  DATA FMT/3H(1H,4H,3A4,4H,A2,,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1
1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF9,,1H ,3HF
29,,1H ,3HF9,,1H ,3HF9,,1H ,1H)/, FB,F0,F1,F2,F3,F4,F5/1H ,2H0,,2H
31,,2H2,,2H3,,2H4,,2H5/,FMT13/2H13/,FMT9X/3H9X/,FMT19/3H19/,
  DATA
  FP/4HP, A,4HTM ,2H ,1H /
1,FT/4HT, D,4HEG K,4H ,2H /,FH/4HH, C,4HAL/G,2H ,1H /
2,FS/4HS, C,4HAL/(,4HG)(K,2H) /,FM/4HM, M,4HOL W,2HT ,1H /
3,FV/4H(DLV,4H/DLP,4H)T ,2H /,FD/4H(DLV,4H/DLT,2H)P,1H /
4,FC/4HCP, ,4HCAL/,4H(G)(,2HK)/,FG/4HGAMM,4HA (S,2H) ,1H /
5,FL/4HSON ,4HVEL,,4HM/SE,2HC /
C
C  INFORMATION USED IN PERFORMANCE OUTPUT
C
  DATA FR1/4HPC/P/, FC1/2HCF/, FN/4HMACH,4H NUM,4HBER ,1H /
1,FR/4HCSTA,4HR, F,4HT/SE,2HC /,FI/4HI, L,4HB-SE,4HC/LB,1H /
2,FA/4HIVAC,4H,LB-,4HSEC/,2HLB /,FA1/4HAE/A/,FA2/1HT/
3,FR1/4HRHOI,2HSP/
  END

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$ORIGIN      F
$*
$IBFTC CECS8  DECK
      SUBROUTINE OUT1
C
      DOUBLE PRECISION G,X
      LOGICAL EQL,FROZ ,TP,HP,SP,HPSP,TPSP,MOLES
C
      DIMENSION NV(13),Z(10,3),HEAD(15),YX(5),YN(5)
C
      COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1  ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2  ,TOTN(13)
      COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
      COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
      COMMON /DOUBLE/ G(20,21), X(20)
      COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEW,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
      COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)
1  ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SS0
      COMMON/OUPT/FMT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1  ,FC(4),FG(4),FB,FMT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
2  ,FR1,FC1,FN(4),FR(4),FA(4),FI(4),FMT9X,F0,FR1(2)
C
      EQUIVALENCE (V,NV),(Z,H0),(IB,FR)
      COMMON/GASES/TAB(3,12,13),NMIX
      COMMON/CASENO/LST
C
      HEAD=(1H ,2A4,5 (A2,F8.5,3X),5 X,F7.5,F13.3,4X,A1,F10.2,F9.4)
C
      DATA HEAD/4H(1H ,4H,2A4,2H,5,4H(A2,,4HF8.5 ,4H,3X),2H,5 ,2HX,
1  ,4HF7.5 ,4H,F13 ,4H,3,4 ,4HX,A1 ,4H,F10 ,4H,2,F ,4H9.4)/

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IMSC/HREC D162424

| | | |
|----|--|-----|
| | DATA FUEL/4HFUEL/,OXID/4HOXID/,ANT/3HANT/,OX/1HO/,IZ/2HOO/ | 340 |
| 1 | ,YN/2H,1, 2H,2, 2H,3, 2H,4, 2H,5 /,F75/4HF7.5/ | 350 |
| 2 | ,YX/3H,57,3H,44,3H,31,3H,18,2H,5 /,F73/4HF7.3/ | 360 |
| | LSP=LST | |
| C | | 370 |
| | IF(KASE.NE.0) WRITE (6,3) KASE | 380 |
| 3 | FORMAT (9H CASE NO. ,I5) | 390 |
| | IF(.NOT.MOLES) WRITE(6,5) | 400 |
| 5 | FORMAT (77X,46HWT FRACTION ENTHALPY STATE TEMP DENSITY/ | 410 |
| 1 | 10X,16HCHEMICAL FORMULA,51X,21H(SEE NOTE) CAL/MOL,10X,5HDEG K, | 420 |
| 2 | 4X,4HG/CC) | 430 |
| | IF(MOLES) WRITE(6,6) | 440 |
| 6 | FORMAT (79X,5HMOLES,7X, 33HENTHALPY STATE TEMP DENSITY/ | 450 |
| 1 | 10X,16HCHEMICAL FORMULA,66X,7HCAL/MOL,10X,13HDEG K G/CC) | 460 |
| | DO 15 N=1,NREAC | 470 |
| | IF(FOX(N).EQ.FOX(N-1))GO TO 11 | 480 |
| | IF(FOX(N).NE.OX)GO TO 10 | 490 |
| | HD1 = OXID | 500 |
| | HD2 = ANT | 510 |
| | GO TO 11 | 520 |
| 10 | HD1 = FUEL | 530 |
| | HD2 = FB | 540 |
| 11 | DO 13 J=1,5 | 550 |
| | IF(NAME(N,J).EQ.IZ.OR.NAME(N,J).EQ.IB) GO TO 14 | 560 |
| 13 | CONTINUE | 570 |
| | J=6 | 580 |
| 14 | J=J-1 | 590 |
| | HEAD(3)=YN(J) | 600 |
| | HEAD(7)=YX(J) | 610 |
| | HEAD(9) = F75 | 620 |
| | IF(PECWT(N).GE.10.) HEAD(9)=F73 | 630 |
| | WRITE(6,HEAD)HD1,HD2,(NAME(N,JJ),ANUM(N,JJ),JJ=1,J),PECWT(N),ENTH(| 640 |
| | 1N), FAZ(N),RTEMP(N),DENS(N) | 650 |
| 15 | CONTINUE | 660 |
| | FPC = 100./(1.+WP(1)) | 670 |
| | WRITE(6,20) WP(1),FPC,EQRAT,RHOP | 680 |
| 20 | FORMAT (1HO,15X, 4HO/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X, | 690 |
| 1 | 19HEQUIVALENCE RATIO=,F7.4,4X,8HDENSITY=,F8.4//) | 700 |

| | | |
|---|---|------|
| C | AGV = 9.80665 | 710 |
| | DO 25 I = 1,NPT | 720 |
| | TOTN(I) = 0 | 730 |
| | DO 25 J = 1,NS | 740 |
| | TOTN(I) = TOTN(I) + EN(J,I) | 750 |
| | 25 CONTINUE | 760 |
| | FMT(4)= FMT(6) | 770 |
| | RETURN | 780 |
| C | | 790 |
| | ENTRY OUT2 | 800 |
| C | | 810 |
| | PRESSURE | 820 |
| C | | 830 |
| | DO 55 I=1,NPT | 840 |
| | K= 2*I+3 | 850 |
| | FMT(K)= F4 | 860 |
| | IF (PPP(I).GE.1.) FMT(K)=F3 | 870 |
| | IF (PPP(I).GE.10.) FMT(K)=F2 | 880 |
| | IF (PPP(I).GE.100.) FMT(K)=F1 | 890 |
| | 55 CONTINUE | 900 |
| | WRITE (6,FMT)(FP(I),I=1,4),(PPP(J),J=1,NPT) | 910 |
| | DO 500 JAB=1,NPT | 920 |
| | 500 TAB(LSP,5,JAB)=PPP(JAB)*14.7*144. | |
| C | | 930 |
| | TEMPERATURE | 940 |
| C | | 950 |
| | DO 65 I=1,NPT | 960 |
| | NV(I)= TTT(I)+.5 | 970 |
| | 65 CONTINUE | 980 |
| | FMT(4)= FMT13 | 990 |
| | FMT(5)= FMT19 | 1000 |
| | WRITE (6,FMT)(FT(I),I=1,4),(NV(J),J=1,NPT) | 1010 |
| | DO 510 JAB=1,NPT | |
| | 510 TAB(LSP,6,JAB)=FLOAT(NV(JAB))*1.8 | |
| C | | 1020 |
| | ENTHALPY | 1030 |
| C | | 1040 |

| | | |
|---|--|------|
| | DO 75 I=1,NPT | 1050 |
| | V(I) = HSUM(I) * R | 1060 |
| | 75 CONTINUE | 1070 |
| | FMT(5)= FB | 1080 |
| | FMT(7)= F1 | 1090 |
| | WRITE (6,FMT)(FH(I),I=1,4),(V(J),J=1,NPT) | 1100 |
| | DO 515 JAB=1,NPT | |
| | 515 TAB(LST,1,JAB)=V(JAB)*1.8*778.*32.174 | |
| C | | 1110 |
| C | ENTROPY | 1120 |
| C | | 1130 |
| | FMT(7)=F4 | 1140 |
| | DO 78 I = 1,NPT | 1150 |
| | V(I) = SSUM(I) * R | 1160 |
| | 78 CONTINUE | 1170 |
| | WRITE (6,FMT)(FS(I),I=1,4),(V(J),J=1,NPT) | 1180 |
| | WRITE (6,80) | 1190 |
| | 80 FORMAT (1H) | 1200 |
| C | | 1210 |
| C | MOLECULAR WEIGHT | 1220 |
| C | | 1230 |
| | FMT(7)= F3 | 1240 |
| | WRITE (6,FMT)(FM(I),I=1,4),(WM(J),J=1,NPT) | 1250 |
| | DO 550 JAB=1,NPT | |
| | 550 TAB(LSP,7,JAB)=WM(JAB) | |
| C | | 1260 |
| C | (DLV/DLP)T | 1270 |
| C | | 1280 |
| | FMT(7)=F5 | 1290 |
| | IF(EQL) WRITE(6,FMT)(FV(I),I=1,4),(DLVPT(J),J=1,NPT) | 1300 |
| C | | 1310 |
| C | (DLV/DLT)P | 1320 |
| C | | 1330 |
| | FMT(7)= F4 | 1340 |
| | IF(EQL) WRITE(6,FMT)(FD(I),I=1,4),(DLVTP(J),J=1,NPT) | 1350 |
| C | | 1360 |
| C | HEAT CAPACITY | 1370 |
| C | | 1380 |

| | | |
|---|--|------|
| | DO 85 I=1,NPT | 1390 |
| | V(I) = CPR(I) * R | 1400 |
| | 85 CONTINUE | 1410 |
| | WRITE(6,FMT)(FC(I),I=1,4),(V(J),J=1,NPT) | 1420 |
| C | | 1430 |
| C | GAMMA(S) | 1440 |
| C | | 1450 |
| | WRITE(6,FMT)(FG(I),I=1,4),(GAMMAS(J),J=1,NPT) | 1460 |
| | DO 540 JAB=1,NPT | |
| | 540 TAB(LSP,3,JAB)=GAMMAS(JAB) | |
| C | | 1470 |
| C | SONIC VELOCITY | 1480 |
| C | | 1490 |
| | FMT(7)= F1 | 1500 |
| | DO 95 I = 1,NPT | 1510 |
| | SONVEL(I) = SQRT(RR*GAMMAS(I)*TTT(I)/WM(I)) | 1520 |
| | 95 CONTINUE | 1530 |
| | WRITE(6,FMT)(FL(I),I=1,4),(SONVEL(J),J=1,NPT) | 1540 |
| | RETURN | 1550 |
| C | | 1560 |
| | ENTRY OUT3 | 1570 |
| | IF(.NOT.EQL) GO TO 331 | 1580 |
| C | | 1590 |
| C | MOLE FRACTIONS - EQUILIBRIUM | 1600 |
| C | | 1610 |
| | WRITE (6,80) | 1620 |
| | FMT(7)= F5 | 1630 |
| | WRITE(6,310) | 1640 |
| | 310 FORMAT(15HOMOLE FRACTIONS //) | 1650 |
| | DO 330 K=1,NS | 1660 |
| | DO 315 I=1,NPT | 1670 |
| | V(I) = EN(K,I) /TOTN(I) | 1680 |
| | 315 CONTINUE | 1690 |
| | DO 316 I=1,NPT | 1700 |
| | IF (V(I).GE.(5.E-6)) GO TO 320 | 1710 |
| | 316 CONTINUE | 1720 |
| | GO TO 330 | 1730 |
| | 320 WRITE (6,FMT) SUB(K,1),SUB(K,2) ,FB,(V(I),I=1,NPT) | 1740 |

| | | |
|------|--|------|
| 330 | CONTINUE | 1750 |
| 331 | WRITE(6,335) | 1760 |
| 335 | FORMAT(118H0ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MO | 1770 |
| | LE FRACTIONS WERE LESS THAN .000005 FOR ALL ASSIGNED CONDITIONS//) | 1780 |
| | LINE= 0 | 1790 |
| | DO 350 K=1,NS | 1800 |
| | DO 340 I=1,NPT | 1810 |
| | IF ((EN(K,I)/TOTN(I)).GE.(5.E-6)) GO TO 343 | 1820 |
| 340 | CONTINUE | 1830 |
| | LINE= LINE+1 | 1840 |
| | Z(LINE,1)= SUB(K,1) | 1850 |
| | Z(LINE,2)= SUB(K,2) | 1860 |
| | Z(LINE,3)= SUB(K,3) | 1870 |
| 343 | IF ((LINE.NE.10) .AND. K.NE.NS) GO TO 350 | 1880 |
| | IF (LINE.EQ.0) GO TO 1000 | 1890 |
| | WRITE(6,345) (Z(LN,1),Z(LN,2),Z(LN,3),LN=1,LINE) | 1900 |
| 345 | FORMAT (10(1X,3A4)) | 1910 |
| | LINE= 0 | 1920 |
| 350 | CONTINUE | 1930 |
| | IF(.NOT.MOLES) WRITE(6,360) | 1940 |
| 360 | FORMAT(78H0NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXI | 1950 |
| | 2DANT IN TOTAL OXIDANTS) | 1960 |
| 1000 | RETURN | 1970 |
| | END | 1980 |

D-111

LMSC/HREC D162424

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$ORIGIN          F
$IBFTC CECS5    DECK
C
SUBROUTINE CPHS
C CALCULATES THERMODYNAMIC PROPERTIES FOR INDIVIDUAL SPECIES
C
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
COMMON/MISC/ENN,SUMN,TT,SO,ATOM(3,101),LLMT(15),BO(15),BOP(15,2)
1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUBO,AC(2),AM(2)
2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  ,RHOP,RMW(15),TLN
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JSI
C
EQUIVALENCE (J,JSI)
C
K = 1
IF(TT,LE,TMID)K = 2
KK = 0
CPSUM=0.
90 IF(COEF(K,1,J).NE.0.)GO TO 97
IF (IUSE(J).LT.0) GO TO 100
KK = K
K = 1
IF (KK.EQ.1) K = 2
97 S(J) = (((COEF(K,5,J)/4.)*TT+ COEF(K,4,J)/3.)*TT+ COEF(K,3,J)/2.
1) * TT+COEF(K,2,J))*TT+ COEF(K,1,J)*TLN + COEF(K,7,J)
HO(J) = (((COEF(K,5,J)/5.)*TT+ COEF(K,4,J)/4.)*TT+ COEF(K,3,J)/3.
1) * TT+ COEF(K,2,J)/2.)*TT+ COEF(K,1,J) + COEF(K,6,J)/TT
CPSUM= CPSUM+(((COEF(K,5,J)*TT+ COEF(K,4,J))*TT+ COEF(K,3,J))*TT
1 + COEF(K,2,J))*TT+ COEF(K,1,J))*EN(J,NPT)
IF (KK.EQ.0) GO TO 100
K = KK
KK = 0
100 IF(J.EQ.NS) GO TO 200
J=J+1
GO TO 90
200 RETURN
END

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LMSC/HREC D162424

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$IBFTC CECS6  DECK
SUBROUTINE MATRIX
C
C
DOUBLE PRECISION G,X
LOGICAL HP,SP,TP,IDEBUG,CONVG,NEWWR
C
COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)
1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)
2 ,TOTN(13)
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HO(150)
1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),BOP(15,2)
1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2)
2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4 ,RHOP,RMW(15),TLN
COMMON /DOUBLE/ G(20,21), X(20)
COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2 ,IONS,NC,INSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
C
EQUIVALENCE (L,NLM)
C
IQ2 = IQ1 + 1
IQ3 = IQ2 + 1
KMAT = IQ3
IF(.NOT.CONVG.AND.TP) KMAT = IQ2
IMAT = KMAT - 1
C
CLEAR MATRIX STORAGES TO ZERO
C
DO 211 I=1,IMAT
DO 211 K=1,KMAT
G(I,K)= 0.0D0
211 CONTINUE
SSS = 0.
HSUM(NPT) = 0.

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|----|---|-----|
| C | | 380 |
| C | BEGIN SET UP OF ITERATION MATRIX | 390 |
| C | | 400 |
| | KK = L | 410 |
| | DO 65 J=1,NS | 420 |
| | H=H0(J)*EN(J,NPT) | 430 |
| | IF (IUSE(J)) 65,11,70 | 440 |
| 11 | F = (H0(J)-S(J)+ENLN(J)+TM)*EN(J,NPT) | 450 |
| | SS = H-F | 460 |
| | TERM1 = H | 470 |
| | IF (KMAT .EQ. IQ2) TERPM1 = F | 480 |
| | DO 55 I = 1, L | 490 |
| C | | 500 |
| C | CALCULATE THE ELEMENTS R(I,K) | 510 |
| C | | 520 |
| | IF (A(I,J) .EQ. 0.) GO TO 55 | 530 |
| | TERM= A(I,J)*EN(J,NPT) | 540 |
| | DO 15 K=I, L | 550 |
| | G(I,K)= G(I,K) + A(K,J)*TERM | 560 |
| 15 | CONTINUE | 570 |
| C | | 580 |
| | G(I,IQ1)=G(I,IQ1)+TERM | 590 |
| | G(I,IQ2)=G(I,IQ2)+A(I,J)*TERM1 | 600 |
| | IF (CONVG .OR. TP) GO TO 55 | 610 |
| | G(I,IQ3)= G(I,IQ3)+A(I,J)*F | 620 |
| | IF (SP) G(IQ2,I) = G(IQ2,I) + A(I,J)*SS | 630 |
| 55 | CONTINUE | 640 |
| | IF (KMAT .EQ. IQ2) GO TO 64 | 650 |
| | IF(CONVG.OR.HP) GO TO 59 | 660 |
| | G(IQ2,IQ1) = G(IQ2,IQ1) + SS | 670 |
| | G(IQ2,IQ2)=G(IQ2,IQ2)+H0(J)*SS | 680 |
| | G(IQ2,IQ3) = G(IQ2,IQ3)+(S(J) - ENLN(J)-TM)*F | 690 |
| | GO TO 62 | 700 |
| 59 | G(IQ2,IQ2)=G(IQ2,IQ2)+H0(J)*H | 710 |
| | IF (CONVG) GO TO 64 | 720 |
| | G(IQ2,IQ3)=G(IQ2,IQ3)+H0(J)*F | 730 |
| 62 | G(IQ1,IQ3)=G(IQ1,IQ3)+F | 740 |
| 64 | G(IQ1,IQ2)=G(IQ1,IQ2)+TERM1 | 750 |

| | | |
|---|--|------|
| | GO TO 65 | 760 |
| C | | 770 |
| C | CONDENSED SPECIES | 780 |
| C | | 790 |
| | 70 KK = KK + 1 | 800 |
| | DO 75 I = 1,L | 810 |
| | G(I, KK) = A(I, J) | 820 |
| | G(I, KMAT) = G(I, KMAT) - A(I, J)*EN(J, NPT) | 830 |
| | 75 CONTINUE | 840 |
| | G(KK, IQ2) = H0(J) | 850 |
| | G(KK, KMAT) = H0(J) - S(J) | 860 |
| | HSUM(NPT) = HSUM(NPT) + H | 870 |
| | IF(.NOT.SP) GO TO 65 | 880 |
| | SSS = SSS + S(J)*EN(J, NPT) | 890 |
| | G(IQ2, KK) = S(J) | 900 |
| | 65 CONTINUE | 910 |
| | SSS = SSS + G(IQ2, IQ1) | 920 |
| | HSUM(NPT) = HSUM(NPT) + G(IQ1, IQ2) | 930 |
| | G(IQ1, IQ1) = SUMN - ENN | 940 |
| C | | 950 |
| C | REFLECT SYMMETRIC PORTIONS OF THE MATRIX | 960 |
| C | | 970 |
| | ISYM = IQ1 | 980 |
| | IF(HP.OR.CONVG) ISYM=IQ2 | 990 |
| | DO 102 I=1, ISYM | 1000 |
| | DO 102 J=I, ISYM | 1010 |
| | G(J, I)=G(I, J) | 1020 |
| | 102 CONTINUE | 1030 |
| C | | 1040 |
| C | COMPLETE THE RIGHT HAND SIDE | 1050 |
| C | | 1060 |
| | IF(CONVG) GO TO 175 | 1070 |
| | DO 145 I=1,L | 1080 |
| | X(1)=B0(I)-G(I, IQ1) | 1090 |
| | G(I, KMAT) = G(I, KMAT)+X(1) | 1100 |
| | 145 CONTINUE | 1110 |
| | G(IQ1, KMAT) = G(IQ1, KMAT)+ENN-SUMN | 1120 |
| C | | 1130 |

| | | |
|-----|--|------|
| C | COMPLETE ENERGY ROW AND TEMPERATURE COLUMN | 1140 |
| C | | 1150 |
| | IF (KMAT .EQ. IQ2) GO TO 185 | 1160 |
| | IF (SP)ENERGY = S0+ENN-SUMN - SSS | 1170 |
| | IF(HP)ENERGY=HSUB0/TT - HSUM(NPT) | 1180 |
| | G(IQ2,IQ3)=G(IQ2,IQ3)+ ENERGY | 1190 |
| 175 | G(IQ2,IQ2)= G(IQ2,IQ2)+CPSUM | 1200 |
| 185 | RETURN | 1210 |
| | END | 1220 |

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|---------|---|--------|-----|
| \$IBFTC | CECS7 | DECK | |
| | SUBROUTINE | MGAUSD | 10 |
| C | | | 20 |
| C | SOLVE ANY LINEAR SET OF UP TO 20 EQUATIONS | | 30 |
| C | | | 40 |
| C | DOUBLE PRECISION G,X,COEFX(20),SUM,Z | | 50 |
| C | | | 60 |
| | COMMON/DOUBLE/G(20,21),X(20) | | 70 |
| | COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM | | 80 |
| | 1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ | | 90 |
| | 2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1 | | 100 |
| C | | | 110 |
| C | EQUIVALENCE (IUSE,IMAT) | | 120 |
| C | | | 130 |
| C | DATA BIGNO/1.E+38/ | | 140 |
| C | | | 150 |
| C | BEGIN ELIMINATION OF NNTH VARIABLE | | 160 |
| C | | | 170 |
| | IUSE1=IUSE+1 | | 180 |
| | 6 DO 45 NN=1,IUSE | | 190 |
| | IF (NN=IUSE) 8,83,8 | | 200 |
| | 83 IF(G(NN,NN))31,23,31 | | 210 |
| C | | | 220 |
| C | SEARCH FOR MAXIMUM COEFFICIENT IN EACH ROW | | 230 |
| C | | | 240 |
| | 8 DO 18 I=NN,IUSE | | 250 |
| | COEFX(I) = BIGNO | | 260 |
| | IF(G(I,NT).EQ.0.) GO TO 18 | | 270 |
| | COEFX(I) = 0. | | 280 |
| | DO 10 J=NN,IUSE1 | | 290 |
| | SUM = G(I,J) | | 300 |
| | IF(SUM.LT.0.) SUM=-SUM | | 310 |
| | IF(J.NE.NN) GO TO 9 | | 320 |
| | Z = SUM | | 330 |
| | GO TO 10 | | 340 |
| | 9 IF(SUM.GT.COEFX(I)) COEFX(I)=SUM | | 350 |
| | 10 CONTINUE | | 360 |
| | COEFX(I) = COEFX(I)/Z | | 370 |

| | | |
|----|--|-----|
| 18 | CONTINUE | 380 |
| | TEMP = BIGNO | 390 |
| | I=0 | 400 |
| 20 | DO 22 J=NN,IUSE | 410 |
| | IF (COEFX(J)-TEMP) 87,22,22 | 420 |
| 87 | TEMP=COEFX(J) | 430 |
| | I=J | 440 |
| 22 | CONTINUE | 450 |
| | IF(I) 28,23,28 | 460 |
| C | | 470 |
| C | INDEX I LOCATES EQUATION TO BE USED FOR ELIMINATING THE NTH | 480 |
| C | VARIABLE FROM THE REMAINING EQUATIONS | 490 |
| C | | 500 |
| C | INTERCHANGE EQUATIONS I AND NN | 510 |
| C | | 520 |
| 28 | IF(NN-1) 29,31,29 | 530 |
| 29 | DO 30 J=NN,IUSE1 | 540 |
| | Z=G(I,J) | 550 |
| | G(I,J)=G(NN,J) | 560 |
| | G(NN,J)=Z | 570 |
| 30 | CONTINUE | 580 |
| C | | 590 |
| C | DIVIDE NTH ROW BY NTH DIAGONAL ELEMENT AND ELIMINATE THE NTH | 600 |
| C | VARIABLE FROM THE REMAINING EQUATIONS | 610 |
| C | | 620 |
| 31 | K = NN + 1 | 630 |
| | DO 36 J = K, IUSE1 | 640 |
| | IF(G(NN,NN).EQ.0.) GO TO 23 | 650 |
| | G(NN,J) = G(NN,J) / G(NN,NN) | 660 |
| 36 | CONTINUE | 670 |
| | IF(K-IUSE1) 88,45,88 | 680 |
| 88 | DO 44 I = K, IUSE | 690 |
| 40 | DO 44 J = K, IUSE1 | 700 |
| | G(I,J) = G(I,J) - G(I,NN)*G(NN,J) | 710 |
| 44 | CONTINUE | 720 |
| 45 | CONTINUE | 730 |
| C | | 740 |
| C | BACKSOLVE FOR THE VARIABLES | 750 |

| | | |
|---|----------------------------|-----|
| C | K = IUSE | 760 |
| | 47 J = K + 1 | 770 |
| | X(K) = 0.0D0 | 780 |
| | SUM = 0.0 | 790 |
| | IF(IUSE - J) 51,48,48 | 800 |
| | 48 DO 50 I = J,IUSE | 810 |
| | SUM = SUM + G(K,I)* X(I) | 820 |
| | 50 CONTINUE | 830 |
| | 51 X(K) = G(K,IUSEI) - SUM | 840 |
| | K = K - 1 | 850 |
| | IF (K) 47,151,47 | 860 |
| | 23 IUSE = IUSE-1 | 870 |
| | 151 RETURN | 880 |
| | END | 890 |
| | | 900 |

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$ORIGIN      E
$IBFTC CECS2  DECK
C                                                    10
    SUBROUTINE REACT                                20
C                                                    30
    DOUBLE PRECISION G,X                            40
    LOGICAL HP,SP,TP, IDEBUG,CONVG,NEWWR, IONS,MOLES,EQL,FROZ 50
C                                                    60
    DIMENSION ANAME(15,5),V(15)                    70
C                                                    80
    COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),B0(15),B0P(15,2) 90
    1 ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPCT,R,RR,HSUB0,AC(2),AM(2) 100
    2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5) 110
    3 ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15) 120
    4 ,RHOP,RMW(15),TLN 130
    COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM 140
    1 ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ 150
    2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1 160
C                                                    170
    EQUIVALENCE (NAME,ANAME),(NLM,L) 180
C                                                    190
    DATA MOL/1HM/,OX/1HO/,LANK/1H /,IZERO/2H00/ 200
    DATA MOLE/1H /
C                                                    210
    DO 10 K=1,2 220
    WP(K)=0. 230
    HPP(K)=0. 240
    RHO(K)=0. 250
    VPLS(K)=0. 260
    VMIN(K)=0. 270
    AC(K)=0. 280
    AM(K)=0. 290
    DO 8 J=1,15 300
    LLMT(J)=0 310
    BOP(J,K)=0. 320
    8 CONTINUE 330
    10 CONTINUE 340
    N=1 350

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|---|-----|
| L=1 | 360 |
| 20 CONTINUE | |
| 21 FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5) | 390 |
| IF(NAME(N,1).EQ.LANK) GO TO 200 | 400 |
| IF(L.EQ.0)GO TO 20 | 410 |
| WRITE (6,31)(NAME(N,I),ANUM(N,I),I=1,5),PECWT(N),MOLE,ENTH(N),FAZ | 420 |
| 1 (N),RTEMP(N),FOX(N),DENS(N) | 430 |
| 31 FORMAT(1X,5(A2,1X,F7.4,2X),F8.4,2X,A1,F11.2,2X,A1,2X,F8.3,2X, | 440 |
| 1A3,3X,F8.5) | |
| 35 IF(MOLE.EQ.MOL) MOLES=.TRUE. | 460 |
| K=2 | 470 |
| IF(FOX(N).EQ.OX)K=1 | 480 |
| DO 38 J=1,15 | 490 |
| DATA(J) = 0. | 500 |
| 38 CONTINUE | 510 |
| RM=0. | 520 |
| DO 100 JJ=1,5 | 530 |
| IF(ANUM(N,JJ).EQ.0.)GO TO 101 | 540 |
| DO 41 J=1,15 | 550 |
| NJ = J | 560 |
| IF(LLMT(J).EQ.0) GO TO 45 | 570 |
| IF(NAME(N,JJ).EQ.LLMT(J))GO TO 46 | 580 |
| 41 CONTINUE | 590 |
| 45 L = NJ | 600 |
| LLMT(J)=NAME(N,JJ) | 610 |
| 46 DO 48 KK=1,101 | 620 |
| IF(ATOM(1,KK).EQ.ANAME(N,JJ))GO TO 50 | 630 |
| 48 CONTINUE | 640 |
| L=0 | 650 |
| GO TO 20 | 660 |
| 50 RM=RM+ANUM(N,JJ)*ATOM(2,KK) | 670 |
| V(J)=ATOM(3,KK) | 680 |
| DATA(J)=ANUM(N,JJ) | 690 |
| 100 CONTINUE | 700 |
| 101 PCWT=PECWT(N) | 710 |
| IF(MOLES) PCWT=PCWT*RM | 720 |
| WP(K)=WP(K) + PCWT | 730 |
| IF(NAME(N,5).NE.IZERO)HPP(K)=HPP(K)+ENTH(N)*PCWT/RM | 740 |

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| | AM(K)=AM(<)+PCWT/RM | 750 |
| | DO 110 J=1,L | 760 |
| | BOP(J,K)=DATA(J)*PCWT/RM +BOP(J,K) | 770 |
| 110 | CONTINUE | 780 |
| | IF(DENS(N).NE.0.)GO TO 115 | 790 |
| | GO TO 117 | 800 |
| 115 | RHO(K)=RHO(K)+PCWT/DENS(N) | 810 |
| 117 | RMW(N) = RM | 820 |
| | N = N+1 | 830 |
| | IF(N.NE.16) GO TO 20 | 840 |
| 200 | NREAC =N-1 | 850 |
| | IF(L.EQ.0) GO TO 1000 | 860 |
| | DO 220 K=1,2 | 870 |
| | IF(WP(K).EQ.0.)GO TO 220 | 880 |
| | HPP(K)=HPP(K)/WP(K) | 890 |
| | AM(K) = WP(K)/AM(K) | 900 |
| | IF(RHO(K).NE.0.)RHO(K)=WP(K)/RHO(K) | 910 |
| | DO 215 J=1,L | 920 |
| | BOP(J,K)=BOP(J,K)/WP(K) | 930 |
| | IF(V(J).LT.0.)VMIN(K)= VMIN(K)+BOP(J,K)*V(J) | 940 |
| | IF(V(J).GT.0.)VPLS(K)=VPLS(K)+BOP(J,K)*V(J) | 950 |
| 215 | CONTINUE | 960 |
| | IF(MOLES) GO TO 220 | 970 |
| | DO 218 N=1,NREAC | 980 |
| | IF(FOX(N).EQ.OX.AND.K.EQ.2) GO TO 218 | 990 |
| | IF(FOX(N).NE.OX.AND.K.EQ.1) GO TO 218 | 1000 |
| | PECWT(N) = PECWT(N)/WP(K) | 1010 |
| 218 | CONTINUE | 1020 |
| 220 | CONTINUE | 1030 |
| | NEWR=.TRUE. | 1040 |
| | DO 230 N = 1,NREAC | 1050 |
| | IF (DENS(N).NE.0.) GO TO 230 | 1060 |
| | RHO (1) = 0. | 1070 |
| | GO TO 1000 | 1080 |
| 230 | CONTINUE | 1090 |
| 1000 | RETURN | 1100 |
| | END | 1110 |

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$IBFTC CECS3
SUBROUTINE SEARCH
C
C SEARCH TAPE FOR THERMO DATA FOR SPECIES TO BE CONSIDERED
  INTEGER SUB,OMIT,END
C
  LOGICAL NEWR
C
  DIMENSION DATE(2,3),MT(4),B(4),OMIT(3,3)
C
  COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
  1  ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
  COMMON/MISC/ENN,SUMN,TT,S0,ATOM(3,10),LLMT(15),B0(15),B0P(15,2)
  1  ,TM,TLOW,TMID,THIGH,PP,CPSUM,OF,EQRAT,FPC,T,R,RR,HSUB0,AC(2),AM(2)
  2  ,HPP(2),RHO(2),VMIN(2),VPLS(2),WP(2),DATA(22),NAME(15,5)
  3  ,ANUM(15,5),PECWT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
  4  ,RHOP,RMW(15),TLN
  COMMON/INDX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,NLM
  1  ,NS,KMAT,IMAT,IQ1,IQ2,NOMIT,IP,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
  2  ,IONS,NC,NSERT,JSOL,JLIQ,KASE,NREAC,IC,JS1
C
  EQUIVALENCE (DATE,EN),(OMIT,ENLN),(ENDD,END),(L,NLM)
  COMMON/TAPE/IPROT
C
  DATA  GAS/1HG/,END/3HEND/
C
  NC= 0
  IX= 0
  COEF(1,1,1) = ENDD
  I = 1
  DO 3 I=1,150
  IF(A(1,I).EQ.ENDD) GO TO 4
  DO 3 J=1,L
  A(J,I) = 0.
  3 CONTINUE
  4 MAXNS = I
  REWIND 8
  REWIND 10

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GO TO 50
IF(IPROT.EQ.1)GO TO 50
READ(8      )TLOW, TMID, THIGH
5 FORMAT (3F10.3)
NS = 1
7 READ(8      ) (SUB(NS, I), I=1, 2), DATE(1, NS), DATE(2, NS), (MT(J), B(J),
1 J=1, 4), PHAZ, T1, T2
10 FORMAT(2A6, 6X, 2A3, 4(A2, F3.0), A1, 2F10.3)
IF(SUB(NS, 1).EQ.END) GO TO 171
READ(8      ) ((COEF(I, J, NS), J=1, 7), I=1, 2)
GO TO 75
50 CONTINUE
READ(10, 5 )TLOW, TMID, THIGH
NS = 1
8 CONTINUE
READ(10, 10) (SUB(NS, I), I=1, 2), DATE(1, NS), DATE(2, NS), (MT(J), B(J),
1 J=1, 4), PHAZ, T1, T2
IF(SUB(NS, 1).EQ.END) GO TO 171
READ(10, 20) ((COEF(I, J, NS), J=1, 7), I=1, 2)
75 CONTINUE
20 FORMAT (5E15.8)
IF(NOMIT.EQ.0) GO TO 810
DO 805 I=1, NOMIT
DO 804 J=1, 3
IF(OMIT(J, I).NE.SUB(NS, J)) GO TO 805
804 CONTINUE
GO TO 8
IF(IPROT.EQ.1)GO TO 8
GO TO 7
805 CONTINUE
810 DO 820 K=1, 4
IF(B(K).EQ.0.) GO TO 825
DO 168 I=1, L
IF(LLMT(I).EQ.MT(K)) GO TO 820
168 CONTINUE
DO 819 J=1, L
819 A(J, NS) = 0.
GO TO 8

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380
410
420
440
450
460
470
480
490
500
510
520
530
540
550
560
570
580

| | | |
|-----|--|-----|
| | IF(IPROT.EQ.1)GO TO 8 | |
| | GO TO 7 | 590 |
| 820 | A(I,NS)= B(K) | 600 |
| 825 | IF(NS.EQ.MAXNS) GO TO 870 | 610 |
| | IUSE(NS)= 0 | 620 |
| | IF(PHAZ.EQ.GAS) GO TO 170 | 630 |
| | NC= NC+1 | 640 |
| | TEMP(NC,1)= T1 | 650 |
| | TEMP(NC,2)= T2 | 660 |
| | IX= IX+1 | 670 |
| | IF(IUSE(NS-1).EQ.0 .OR. NC.EQ.1) GO TO 145 | 680 |
| | DO 830 I=1,L | 690 |
| | IF(A(I,NS).NE.A(I,NS-1)) GO TO 145 | 700 |
| 830 | CONTINUE | 710 |
| | IX= IX-1 | 720 |
| 145 | IUSE(NS)= -IX | 730 |
| 170 | NS= NS+1 | 740 |
| | GO TO 8 | |
| | IF(IPROT.EQ.1)GO TO 8 | |
| | GO TO 7 | 750 |
| 870 | WRITE(6,871) (SUB(NS,J),J=1,2) | |
| 871 | FORMAT (45HODIMENSIONS IN/SPECES/TOO SMALL TO CONSIDER ,2A6) | 770 |
| | GO TO 8 | |
| | IF(IPROT.EQ.1)GO TO 8 | |
| | GO TO 7 | 780 |
| 171 | NS= NS-1 | 790 |
| | NEWR= .FALSE. | 800 |
| | WRITE(6,172) | 810 |
| 172 | FORMAT(42HOSPECIES BEING CONSIDERED IN THIS SYSTEM | 820 |
| | DO 174 I=1,NS,5 | 830 |
| | I5= I+4 | 840 |
| | IF(NS.LT.I5) I5=NS | 850 |
| 174 | WRITE (6,176)(DATE(1,J),DATE(2,J),SUB(J,1),SUB(J,2) | 8 |
| | 1 I5) | 870 |
| 176 | FORMAT(5(5X,2A3,2X,2A6)) | 88 |
| | RETURN | 890 |
| | END | 900 |

```

$DATA
      3      3      0      0      0      0      1
+0.0314    +0.1      +20.0      +0.0
+0.314     +20.      +0.0      +100.
H +13.0220  2.17040N  4.34070
N 2.173600  4.3472
      10.      11.      12.      1.0

```

```

F L      .5      -5900.      298.15
O L      .5      +27560.      298.15

```

(2) MIX= 2 (1) TRIAL RUN SIMULATION SELECTION
NPTS= 5 IP= 0 IT= 0 IG= 0 IFLG1= 0 ITYPE= 1

(3) NOZZLE GEOMETRY FOLLOWS

| THRUST AREA | THRUST RADIUS | AREA RATIO | LIP ANGLE |
|-------------|---------------|------------|-----------|
| 0.314E-01 | 0.100E 00 | 0.200E 02 | 0.000E-38 |

(4) - - - - -

INITIAL CHAMBER TEMP= 0.100E 04 PRESSURE= 0.200E 03

(5) PROTOTYPE INFORMATION
RADP= 0.314E 00AETP= 0.200E 02ANGP= 0.000E-38PREP= 0.100E 03

(6) REGION OF PLUME TO BE DUPLICATED
XP1= 0.100E 02 XP2= 0.110E 02 XP3= 0.120E 02

(7)
ERROR MULTIPLICATION FACTOR = 0.100E 01

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LMSC/HREC D162424

(8) THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

PC = 100.0 PSIA
 JAS = V0 *****

CHEMICAL FORMULA
 FUEL H ***** 0 2.17040 4 34070
 OXIDANT N 2 17350 0 + 34720

WT FRACTION ENTHALPY STATE TEMP DENSITY
 (S= NOTE) CAL/MOL DEG K G/CC
 ***** -5900.000 L 298.15 -0.0000
 ***** 27560.000 L 298.15 -0.0000

Ø/F = 1.0000 PERCENT FUEL = 50.0000 EQUIVALENC RATIO = 0.9445 DENSITY = -0.0000

| | CHAMBER | THRUST | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT |
|-----------------|---------|--------|--------|---------|---------|---------|---------|---------|---------|---------|---------|---------|---------|
| P, ATM | 1.000 | 1.787 | 25.000 | 300.000 | 1000.00 | 2000.00 | 3000.00 | 4000.00 | 5000.00 | 7000.00 | 10000.0 | 30000.0 | 60000.0 |
| T, DEG K | 5.805 | 3.807 | 0.2722 | 0.0227 | 0.0068 | 0.0034 | 0.0023 | 0.0017 | 0.0014 | 0.0010 | 0.0007 | 0.0002 | 0.0001 |
| W, CAL/G | 3140 | 2324 | 1701 | 994 | 748 | 629 | 568 | 527 | 498 | 456 | 415 | 310 | 257 |
| S, CAL/(G)(K) | 110.7 | -61.6 | -545.6 | -973.2 | -1077.2 | -1124.6 | -1148.7 | -1154.4 | -1175.8 | -1191.7 | -1207.2 | -1246.5 | -1266.1 |
| M, MOL WT | 3.868 | 3.1358 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 | 3.1868 |
| CP, CAL/(G)(K) | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 | 19.961 |
| GAMMA (S) | 0.5484 | 0.5408 | 0.4921 | 0.4324 | 0.4056 | 0.3947 | 0.3890 | 0.3855 | 0.3831 | 0.3799 | 0.3771 | 0.3718 | 0.3703 |
| SNR VEL, M/SEC | 1.2218 | 1.2256 | 1.2596 | 1.2991 | 1.3243 | 1.3373 | 1.3440 | 1.3482 | 1.3511 | 1.3551 | 1.3586 | 1.3657 | 1.3678 |
| MACH NUMBER | 1254.1 | 1200.7 | 942.5 | 734.0 | 542.3 | 592.1 | 565.8 | 544.2 | 529.2 | 507.3 | 484.6 | 419.8 | 382.9 |
| CSTAR, FT/SEC | 0.000 | 1.000 | 2.670 | 4.103 | 4.909 | 5.430 | 5.758 | 6.003 | 6.199 | 6.508 | 6.852 | 8.027 | 9.866 |
| CF | 57+5 | 5745 | 57+5 | 5745 | 5745 | 5745 | 5745 | 5745 | 5745 | 5745 | 5745 | 5745 | 5745 |
| AE/AT | 0.688 | 1.437 | 1.720 | 1.800 | 1.836 | 1.854 | 1.865 | 1.874 | 1.885 | 1.896 | 1.925 | 1.938 | 1.938 |
| IVAC, LB-SEC/LB | 1.000 | 4.020 | 23.59 | 55.43 | 93.14 | 124.8 | 153.6 | 180.4 | 229.9 | 297.3 | 656.1 | 1081.7 | 1081.7 |
| I, LB-SEC/LB | 222.3 | 285.2 | 321.1 | 331.6 | 338.2 | 338.5 | 339.9 | 341.0 | 342.5 | 343.9 | 347.6 | 349.3 | 349.3 |
| RHOISP | 122.4 | 256.5 | 307.1 | 321.5 | 327.8 | 331.0 | 333.1 | 334.6 | 336.6 | 338.6 | 343.6 | 346.1 | 346.1 |
| | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 | -0.0 |

MOLE FRACTIONS

| | H2 | H2O | N2 | NH3 | NH4 | N2O | N2O4 |
|---|-----------|-----------|---------|---------|---------|-----|------|
| 1 | 0.736E-01 | 0.736E-01 | | | | | |
| + | 0.02+50 | 0.482E 00 | 0.00003 | 0.07356 | 0.48203 | | |
| V | 0.00001 | 0.301E 00 | 0.30077 | 0.01412 | 0.00001 | | |
| Ø | 0.01225 | 0.504E-01 | 0.03036 | 0.03222 | | | |

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN 0.00005 FOR ALL ASSIGNED CONDITIONS

H2O H2O2 NH3 NH4 N2O N2O4

NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

(9)

| H FT2/S2 | A/A# | GAMMA | M VØ. | P PSF | T DEG R | MØL WT |
|------------|------------|-----------|-----------|-----------|-----------|-----------|
| 0,499E 07 | -0,000E- 9 | 0,122E 01 | 0,000E-35 | 0,144E 00 | 0,565E 04 | 0,200E 02 |
| -0,273E 07 | 0,100E 01 | 0,122E 01 | 0,100E 01 | 0,806E 04 | 0,508E 04 | 0,200E 02 |
| -0,271E 04 | 0,402E 0 | 0,125E 01 | 0,267E 01 | 0,576E 01 | 0,306E 04 | 0,200E 02 |

(10)

PROTOTYPE EXIT PLANE REYNOLDS NØ. IS 0,230E 05

(11)

ORIGIN OF SOURCE FLOW AT X=-0,121E 00

(12)

WITH THETA= 0,148E 01

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| (13) | (14) | (15) | (16) | (17) | (18) | (19) | (20) | (21) |
|------|---------|-------|-------|------------|------|------|------|------|
| S2 | MACH NØ | R± NØ | GAMMA | KNUDS=N NØ | TØ | T | PO | P |

| | | | | | | | | |
|------------|------------|------------|------------|------------|------------|------------|------------|------------|
| 0,4809E 01 | 0,4793E 01 | 0,3874E 05 | 0,1522E 01 | 0,1415E-04 | 0,7124E 04 | 0,1598E 04 | 0,6535E 04 | 0,6018E 02 |
| 0,7617E 01 | 0,5774E 01 | 0,0129E 05 | 0,1344E 01 | 0,4561E-03 | 0,7124E 04 | 0,1018E 04 | 0,6585E 04 | 0,2535E 02 |
| 0,1043E 01 | 0,6585E 01 | 0,5232E 05 | 0,1356E 01 | 0,7523E-03 | 0,7124E 04 | 0,8038E 03 | 0,6585E 04 | 0,7098E 01 |

(22) PROTOTYPE CONDENSATION OCCURS AT 0,502E 03

LMSC/HREC D162424

(23) THERMAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

AT ALL ASSIGNED TEMPERATURE

P0 = 200.0 PSIA
CAS NO. 1

| CHEMICAL FORMULA | |
|------------------|---------------------|
| FJ L | C 1.00000 F 4.00000 |
| FJ L | V 2.00000 |
| FJ L | C 1.00000 J 2.00000 |

| WT FRACTION (SEE NOTE) | ENTHALPY CAL/MOL | STATE | TEMP DEG K | DENSITY G/CC |
|---------------------------|---------------------|-------|---------------|-----------------|
| ***** | -217200.000 | G | 298.15 | -0.0000 |
| ***** | 0.000 | G | 298.15 | -0.0000 |
| ***** | -94051.800 | G | 298.15 | -0.0000 |

W/F = 0.0000 PERCENT FULL = ***** EQUIVALENCE RATIO = 1.0000 DENSITY = 0.0000

| | CHAMBER | THROAT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT | EXIT |
|-----------------|---------|---------|---------|---------|---------|---------|---------|---------|---------|---------|
| P0/P | 1.000 | 1.776 | 25.000 | 300.000 | 1000.00 | 2000.00 | 3000.00 | 4000.00 | 5000.00 | 7000.00 |
| P, ATM | 13.61 | 7.664 | 0.5444 | 0.0454 | 0.0136 | 0.0068 | 0.0045 | 0.0034 | 0.0027 | 0.0019 |
| T, DEG K | 1000 | 907 | 563 | 339 | 208 | 219 | 198 | 184 | 174 | 159 |
| T, CAL/G | -1242.2 | -1267.7 | -1356.7 | -1408.0 | -1424.6 | -1432.3 | -1436.2 | -1438.8 | -1440.6 | -1443.2 |
| S, CAL/(G)(K) | 1.4026 | 1.4026 | 1.4026 | 1.4026 | 1.4026 | 1.4026 | 1.4026 | 1.4026 | 1.4026 | 1.4026 |
| M, MOL WT | +2.793 | +2.793 | 42.793 | 42.793 | 42.793 | 42.793 | 42.793 | 42.793 | 42.793 | 42.793 |
| CP, CAL/(G)(K) | 0.2767 | 0.2715 | 0.2434 | 0.2123 | 0.1977 | 0.1898 | 0.1855 | 0.1825 | 0.1803 | 0.1770 |
| GAMMA (S) | 1.2017 | 1.2053 | 1.2358 | 1.2799 | 1.3070 | 1.3238 | 1.3340 | 1.3413 | 1.3470 | 1.3556 |
| SON VCL, M/SEC | 483.2 | +61.1 | 367.8 | 290.5 | 256.1 | 237.2 | 226.5 | 219.0 | 213.3 | 204.8 |
| MACH NUMBER | 0.000 | 1.000 | 2.660 | 4.054 | 5.823 | 5.316 | 5.625 | 5.955 | 6.041 | 6.332 |
| QSTAR, FT/SEC | | 2227 | 2227 | 2227 | 2227 | 2227 | 2227 | 2227 | 2227 | 2227 |
| QF | | 0.579 | 442 | 1.735 | 1.820 | 1.858 | 1.877 | 1.889 | 1.898 | 1.910 |
| AE/AT | | 1.000 | 1.120 | 14.75 | 59.85 | 99.32 | 133.4 | 154.3 | 193.1 | 246.1 |
| IVAC, LB-SEC/LB | | 86.0 | 111.2 | 125.8 | 130.1 | 132.0 | 133.0 | 133.6 | 134.1 | 134.7 |
| I, LB-SEC/LB | | 47.0 | 99.2 | 120.1 | 126.0 | 128.6 | 129.9 | 130.8 | 131.4 | 132.2 |
| RATISP | | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 | 0.0 |

MOLE FRACTIONS

| | 1 | CF4 | CF4 | 0.145E 00 | 0.145E 00 |
|-----|------|---------|-----|-----------|-----------|
| | | CF2 | CF2 | 0.995E-01 | 0.995E-01 |
| | | C2 | C2 | 0.145E 00 | 0.145E 00 |
| | | V2 | V2 | 0.611E 00 | 0.611E 00 |
| CF+ | Q000 | 0.14475 | CF2 | Q000 | 0.09951 |
| | | | C2 | Q000 | 0.14471 |
| | | | N2 | Q000 | 0.61103 |

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .000005 FOR ALL ASSIGNED CONDITIONS

| | | | | | | | | | | | | | | | | | | | | | |
|-----|------|------|------|-----|------|-----|------|-----|------|-----|------|-----|------|-----|------|-----|------|----|------|------|------|
| (S) | Q000 | CF | Q000 | CF2 | Q000 | CF2 | Q000 | CN | Q000 | CN2 | Q000 | CN | Q000 | CF | Q000 | CF | Q000 | C2 | Q000 | C2F2 | Q000 |
| C | Q000 | C2N2 | Q000 | C2O | Q000 | C2 | Q000 | F | Q000 | FCN | Q000 | F | Q000 | F | Q000 | F2 | Q000 | F2 | Q000 | N | Q000 |
| V | Q000 | NF2 | Q000 | NF2 | Q000 | N | Q000 | N2F | Q000 | N2 | Q000 | N2F | Q000 | N2F | Q000 | N2C | Q000 | N2 | Q000 | N2 | Q000 |
| | Q000 | O2 | Q000 | | | | | | | | | | | | | | | | | | |

NOTE- WEIGHT FRACTION OF FJL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

(24)

(30) TABLE OF THERMODYNAMIC PROPERTIES FOR MIXTURE

| H FT ² /S ² | A/A* | GAMMA | M NØ. | P PSF | T DEG R | MØL WT |
|-----------------------------------|-------------|-----------|------------|-----------|-----------|-----------|
| -0.560E 03 | -0.000E -19 | 0.120E 01 | 0.000E -33 | 0.289E 05 | 0.180E 04 | 0.428E 02 |
| -0.571E 03 | 0.100E 01 | 0.121E 01 | 0.100E 01 | 0.162E 05 | 0.153E 04 | 0.428E 02 |
| -0.581E 03 | 0.412E 01 | 0.124E 01 | 0.265E 01 | 0.115E 04 | 0.101E 04 | 0.428E 02 |
| -0.534E 04 | 0.247E 02 | 0.128E 01 | 0.407E 01 | 0.960E 02 | 0.610E 03 | 0.428E 02 |

(25)

TABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 1

| H FT ² /S ² | A/A* | GAMMA | M NØ. | P PSF | T DEG R | MØL WT |
|-----------------------------------|-------------|-----------|------------|-----------|-----------|-----------|
| -0.101E 09 | -0.000E -19 | 0.111E 01 | 0.000E -38 | 0.288E 05 | 0.180E 04 | 0.733E 02 |
| -0.102E 09 | 0.100E 01 | 0.111E 01 | 0.100E 01 | 0.168E 05 | 0.170E 04 | 0.733E 02 |
| -0.105E 09 | 0.483E 01 | 0.112E 01 | 0.261E 01 | 0.115E 04 | 0.129E 04 | 0.733E 02 |
| -0.107E 09 | 0.350E 02 | 0.113E 01 | 0.374E 01 | 0.960E 02 | 0.977E 03 | 0.733E 02 |

(26)

TABLE OF THERMODYNAMIC PROPERTIES FOR COMPONENT 2

| H FT ² /S ² | A/A* | GAMMA | M NØ. | P PSF | T DEG R | MØL WT |
|-----------------------------------|-------------|-----------|------------|-----------|-----------|-----------|
| -0.110E 08 | -0.000E -19 | 0.130E 01 | 0.000E -38 | 0.288E 05 | 0.180E 04 | 0.302E 02 |
| -0.127E 08 | 0.100E 01 | 0.132E 01 | 0.100E 01 | 0.156E 05 | 0.150E 04 | 0.302E 02 |
| -0.175E 08 | 0.354E 01 | 0.130E 01 | 0.271E 01 | 0.115E 04 | 0.805E 03 | 0.302E 02 |
| -0.200E 08 | 0.184E 02 | 0.139E 01 | 0.440E 01 | 0.960E 02 | 0.407E 03 | 0.302E 02 |
| -0.207E 08 | 0.423E 02 | 0.139E 01 | 0.539E 01 | 0.288E 02 | 0.292E 03 | 0.302E 02 |

SIMULANT RN AT EXIT = 0.104E 06

GROUP 11

- ORIGIN OF SOURCE FLOW AT X= 0.136E-01 WITH THETA= 0.160E 01

GROUP 12

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| S2 | MACH NØ | RE NØ | GAMMA | KNUDSEN NØ | TØ | T | PO | P |
|------------|------------|------------|------------|------------|------------|------------|------------|------------|
| 0.1394E 01 | 0.4681E 01 | 0.5738E 08 | 0.1304E 01 | 0.2587E-05 | 0.2113E 04 | 0.4878E 03 | 0.1923E 05 | 0.1278E 03 |
| 0.2239E 01 | 0.5592E 01 | 0.8812E 07 | 0.1333E 01 | 0.8181E-05 | 0.2236E 04 | 0.3602E 03 | 0.1494E 05 | 0.3548E 02 |
| 0.3183E 01 | 0.6433E 01 | 0.4103E 07 | 0.1356E 01 | 0.2129E-04 | 0.2331E 04 | 0.2785E 03 | 0.1221E 05 | 0.9935E 01 |
| 0.4078E 01 | 0.7105E 01 | 0.2753E 07 | 0.1356E 01 | 0.3494E-04 | 0.2331E 04 | 0.2336E 03 | 0.1221E 05 | 0.3676E 01 |

SIMULANT CONDENSATION PT. IS 0.225E 02