

Ceredo Title V Renewal

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Mr. Moats,

Attached are our comments for R30-09900013-2022. Engine G3 has a bhp of 812 and we plan to update this in a R13 application.

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2 attachments

DPPermit R30-09900013-2022-ERM Comments.docx 312K

DPFactSheet R30-09900013-2022_ERM Comments.doc 114K

West Virginia Department of Environmental Protection Division of Air Quality

> Harold D. Ward Cabinet Secretary

Permit to Operate



Pursuant to **Title V** of the Clean Air Act

Issued to:

Columbia Gas Transmission, LLC Ceredo Compressor Station R30-09900013-2022

Laura M. Crowder Director, Division of Air Quality

Issued: Draft/Proposed • Effective: Draft/Proposed Expiration: Draft/Proposed • Renewal Application Due: Draft/Proposed

Permit Number: **R30-09900013-2022** Permittee: **Columbia Gas Transmission, LLC** Facility Name: **Ceredo Compressor Station** Permittee Mailing Address: **1700 MacCorkle Avenue, SE, Charleston, WV 25314**

This permit is issued in accordance with the West Virginia Air Pollution Control Act (West Virginia Code §§ 22-5-1 et seq.) and 45CSR30 — Requirements for Operating Permits. The permittee identified at the above-referenced facility is authorized to operate the stationary sources of air pollutants identified herein in accordance with all terms and conditions of this permit.

Facility Location:	Ceredo, Wayne County, West Virginia		
Facility Mailing Address:	1664 Walkers Branch Road, Huntington, WV 25704		
Telephone Number:	(304) 453-7502		
Type of Business Entity:	LLC		
Facility Description:	Natural Gas Compressor Station		
SIC Codes:	4922		
UTM Coordinates:	366.1 km Easting • 4247.7 km Northing • Zone 17		

Permit Writer: Nikki Moats

Any person whose interest may be affected, including, but not necessarily limited to, the applicant and any person who participated in the public comment process, by a permit issued, modified or denied by the Secretary may appeal such action of the Secretary to the Air Quality Board pursuant to article one [§§ 22B-1-1 et seq.], Chapter 22B of the Code of West Virginia. West Virginia Code §22-5-14.

Issuance of this Title V Operating Permit does not supersede or invalidate any existing permits under 45CSR13, 14 or 19, although all applicable requirements from such permits governing the facility's operation and compliance have been incorporated into the Title V Operating Permit.

Table of Contents

1.0	Emission Units and Active R13, R14, and R19 Permits
2.0	General Conditions4
3.0	Facility-Wide Requirements13
4.0	Source Specific Requirements [emission point ID(s): BL3, H1, H3]
5.0	Source Specific Requirements [emission point ID(s): E01, E02, E03, E04, E05, E06, E07, G3, G4]
6.0	Source Specific Requirements [emission point ID(s): E10]

1.0 Emission Units and Active R13, R14, and R19 Permits

Emission Units 1.1.

Emission Unit ID	Emission Point ID	Emission Unit Description	Year Installed	Design Capacity	Control Device
00501	E01	Reciprocating Engine/Integral Compressor; Cooper- Bessemer GMWH-8; 2-cycle, lean burn	1954	2,800 HP	N/A
00502	E02	Reciprocating Engine/Integral Compressor; Cooper- Bessemer GMWH-8; 2-cycle, lean burn	1954	2,800 HP	N/A
00503	E03	Reciprocating Engine/Integral Compressor; Cooper- Bessemer GMWH-8; 2-cycle, lean burn	1954	2,800 HP	N/A
00504	E04	Reciprocating Engine/Integral Compressor; Cooper- Bessemer GMWH-8; 2-cycle, lean burn	1957	2,800 HP	N/A
00505	E05	Reciprocating Engine/Integral Compressor; Cooper- Bessemer GMWH-8; 2-cycle, lean burn	1958	2,800 HP	N/A
00506	E06	Reciprocating Engine/Integral Compressor; Cooper- Bessemer GMWH-8; 2-cycle, lean burn	1960	2,800 HP	N/A
00507	E07	Reciprocating Engine/Integral Compressor; Cooper- Bessemer 8V-250; 2-cycle, lean burn	1965	2,700 HP	N/A
00510	E10	Solar Titan 250 Combustion Turbine	2018	30,399 HP	SoloNO _x
005G3	G3	Reciprocating Engine/Generator; Waukesha F3521GL; 4-cycle, lean burn; emergency	1996	812 HP	N/A
005G4	G4	Waukesha VGF-P48GL Emergency Generator	2017	1,175 HP	N/A
BLR3	BL3	BL3 Hurst S-4-G-150-15 Boiler		6.276 MMBtu/hr	N/A
HTR1	H1	Fuel Gas Heater	1998	0.375 MMBtu/hr	N/A
HTR3	Н3	Heater	2017	0.60 MMBtu/hr	NA
n/a	n/a	Oil-Water Storage Tank	2017	900 Gallons	None
n/a	n/a	Waste Water Storage Tank	2017	5,000 Gallons	None
n/a	n/a	Condensate Storage Tank	2017	5,000 Gallons	None

1.2. Active R13, R14, and R19 Permits

The underlying authority for any conditions from R13, R14, and/or R19 permits contained in this operating permit is cited using the original permit number (e.g. R13-1234). The current applicable version of such permit(s) is listed below.

Permit Number	Date of Issuance
R13-1856C	December 18, 2017

West Virginia Department of Environmental Protection • Division of Air Quality Approved: Draft/Proposed • Modified: N/A

2.0 General Conditions

2.1. Definitions

- 2.1.1. All references to the "West Virginia Air Pollution Control Act" or the "Air Pollution Control Act" mean those provisions contained in W.Va. Code §§ 22-5-1 to 22-5-18.
- 2.1.2. The "Clean Air Act" means those provisions contained in 42 U.S.C. §§ 7401 to 7671q, and regulations promulgated thereunder.
- 2.1.3. "Secretary" means the Secretary of the Department of Environmental Protection or such other person to whom the Secretary has delegated authority or duties pursuant to W.Va. Code §§ 22-1-6 or 22-1-8 (45CSR§30-2.12.). The Director of the Division of Air Quality is the Secretary's designated representative for the purposes of this permit.
- 2.1.4. Unless otherwise specified in a permit condition or underlying rule or regulation, all references to a "rolling yearly total" shall mean the sum of the monthly data, values or parameters being measured, monitored, or recorded, at any given time for the previous twelve (12) consecutive calendar months.

2.2. Acronyms

CAAA	Clean Air Act Amendments	NSPS	New Source Performance
CBI	Confidential Business Information		Standards
CEM	Continuous Emission Monitor	PM	Particulate Matter
CES	Certified Emission Statement	PM_{10}	Particulate Matter less than
C.F.R. or CFR	Code of Federal Regulations		10µm in diameter
CO	Carbon Monoxide	pph	Pounds per Hour
C.S.R. or CSR	Codes of State Rules	ppm	Parts per Million
DAQ	Division of Air Quality	PSD	Prevention of Significant
DEP	Department of Environmental		Deterioration
	Protection	psi	Pounds per Square Inch
FOIA	Freedom of Information Act	ŜIC	Standard Industrial
HAP	Hazardous Air Pollutant		Classification
HON	Hazardous Organic NESHAP	SIP	State Implementation Plan
HP	Horsepower	SO_2	Sulfur Dioxide
lbs/hr <i>or</i> lb/hr	Pounds per Hour	ТАР	Toxic Air Pollutant
LDAR	Leak Detection and Repair	TPY	Tons per Year
m	Thousand	TRS	Total Reduced Sulfur
MACT	Maximum Achievable Control	TSP	Total Suspended Particulate
	Technology	USEPA	United States
mm	Million		Environmental Protection
mmBtu/hr	Million British Thermal Units per		Agency
	Hour	UTM	Universal Transverse
mmft³/hr <i>or</i>	Million Cubic Feet Burned per		Mercator
mmcf/hr	Hour	VEE	Visual Emissions
NA or N/A	Not Applicable		Evaluation
NAAQS	National Ambient Air Quality	VOC	Volatile Organic
	Standards		Compounds
NESHAPS	National Emissions Standards for		*
	Hazardous Air Pollutants		
NO _x	Nitrogen Oxides		

2.3. Permit Expiration and Renewal

- 2.3.1. Permit duration. This permit is issued for a fixed term of five (5) years and shall expire on the date specified on the cover of this permit, except as provided in 45CSR§30-6.3.b. and 45CSR§30-6.3.c.
 [45CSR§30-5.1.b.]
- 2.3.2. A permit renewal application is timely if it is submitted at least six (6) months prior to the date of permit expiration.
 [45CSR§30-4.1.a.3.]
- 2.3.3. Permit expiration terminates the source's right to operate unless a timely and complete renewal application has been submitted consistent with 45CSR§30-6.2. and 45CSR§30-4.1.a.3.
 [45CSR§30-6.3.b.]
- 2.3.4. If the Secretary fails to take final action to deny or approve a timely and complete permit application before the end of the term of the previous permit, the permit shall not expire until the renewal permit has been issued or denied, and any permit shield granted for the permit shall continue in effect during that time. [45CSR§30-6.3.c.]

2.4. Permit Actions

2.4.1. This permit may be modified, revoked, reopened and reissued, or terminated for cause. The filing of a request by the permittee for a permit modification, revocation and reissuance, or termination, or of a notification of planned changes or anticipated noncompliance does not stay any permit condition.
 [45CSR§30-5.1.f.3.]

2.5. Reopening for Cause

- 2.5.1. This permit shall be reopened and revised under any of the following circumstances:
 - a. Additional applicable requirements under the Clean Air Act or the Secretary's legislative rules become applicable to a major source with a remaining permit term of three (3) or more years. Such a reopening shall be completed not later than eighteen (18) months after promulgation of the applicable requirement. No such reopening is required if the effective date of the requirement is later than the date on which the permit is due to expire, unless the original permit or any of its terms and conditions has been extended pursuant to 45CSR§§30-6.6.a.1.A. or B.
 - b. Additional requirements (including excess emissions requirements) become applicable to an affected source under Title IV of the Clean Air Act (Acid Deposition Control) or other legislative rules of the Secretary. Upon approval by U.S. EPA, excess emissions offset plans shall be incorporated into the permit.
 - c. The Secretary or U.S. EPA determines that the permit contains a material mistake or that inaccurate statements were made in establishing the emissions standards or other terms or conditions of the permit.
 - d. The Secretary or U.S. EPA determines that the permit must be revised or revoked and reissued to assure compliance with the applicable requirements.

[45CSR§30-6.6.a.]

2.6. Administrative Permit Amendments

2.6.1. The permittee may request an administrative permit amendment as defined in and according to the procedures specified in 45CSR§30-6.4.
 [45CSR§30-6.4.]

2.7. Minor Permit Modifications

2.7.1. The permittee may request a minor permit modification as defined in and according to the procedures specified in 45CSR§30-6.5.a.
 [45CSR§30-6.5.a.]

2.8. Significant Permit Modification

2.8.1. The permittee may request a significant permit modification, in accordance with 45CSR§30-6.5.b., for permit modifications that do not qualify for minor permit modifications or as administrative amendments.
 [45CSR§30-6.5.b.]

2.9. Emissions Trading

2.9.1. No permit revision shall be required, under any approved economic incentives, marketable permits, emissions trading, and other similar programs or processes for changes that are provided for in the permit and that are in accordance with all applicable requirements.
 [45CSR\$30-5.1.h.]

2.10. Off-Permit Changes

- 2.10.1. Except as provided below, a facility may make any change in its operations or emissions that is not addressed nor prohibited in its permit and which is not considered to be construction nor modification under any rule promulgated by the Secretary without obtaining an amendment or modification of its permit. Such changes shall be subject to the following requirements and restrictions:
 - a. The change must meet all applicable requirements and may not violate any existing permit term or condition.
 - b. The permittee must provide a written notice of the change to the Secretary and to U.S. EPA within two (2) business days following the date of the change. Such written notice shall describe each such change, including the date, any change in emissions, pollutants emitted, and any applicable requirement that would apply as a result of the change.
 - c. The change shall not qualify for the permit shield.
 - d. The permittee shall keep records describing all changes made at the source that result in emissions of regulated air pollutants, but not otherwise regulated under the permit, and the emissions resulting from those changes.
 - e. No permittee may make any change subject to any requirement under Title IV of the Clean Air Act (Acid Deposition Control) pursuant to the provisions of 45CSR§30-5.9.

f. No permittee may make any changes which would require preconstruction review under any provision of Title I of the Clean Air Act (including 45CSR14 and 45CSR19) pursuant to the provisions of 45CSR§30-5.9.

[45CSR§30-5.9.]

2.11. Operational Flexibility

- 2.11.1. The permittee may make changes within the facility as provided by § 502(b)(10) of the Clean Air Act. Such operational flexibility shall be provided in the permit in conformance with the permit application and applicable requirements. No such changes shall be a modification under any rule or any provision of Title I of the Clean Air Act (including 45CSR14 and 45CSR19) promulgated by the Secretary in accordance with Title I of the Clean Air Act and the change shall not result in a level of emissions exceeding the emissions allowable under the permit.
 [45CSR§30-5.8]
- 2.11.2. Before making a change under 45CSR§30-5.8., the permittee shall provide advance written notice to the Secretary and to U.S. EPA, describing the change to be made, the date on which the change will occur, any changes in emissions, and any permit terms and conditions that are affected. The permittee shall thereafter maintain a copy of the notice with the permit, and the Secretary shall place a copy with the permit in the public file. The written notice shall be provided to the Secretary and U.S. EPA at least seven (7) days prior to the date that the change is to be made, except that this period may be shortened or eliminated as necessary for a change that must be implemented more quickly to address unanticipated conditions posing a significant health, safety, or environmental hazard. If less than seven (7) days notice is provide because of a need to respond more quickly to such unanticipated conditions, the permittee shall provide notice to the Secretary and U.S. EPA as soon as possible after learning of the need to make the change. [45CSR§30-5.8.a.]
- 2.11.3. The permit shield shall not apply to changes made under 45CSR§30-5.8., except those provided for in 45CSR§30-5.8.d. However, the protection of the permit shield will continue to apply to operations and emissions that are not affected by the change, provided that the permittee complies with the terms and conditions of the permit applicable to such operations and emissions. The permit shield may be reinstated for emissions and operations affected by the change:
 - a. If subsequent changes cause the facility's operations and emissions to revert to those authorized in the permit and the permittee resumes compliance with the terms and conditions of the permit, or
 - b. If the permittee obtains final approval of a significant modification to the permit to incorporate the change in the permit.

[45CSR§30-5.8.c.]

2.11.4. "Section 502(b)(10) changes" are changes that contravene an express permit term. Such changes do not include changes that would violate applicable requirements or contravene enforceable permit terms and conditions that are monitoring (including test methods), recordkeeping, reporting, or compliance certification requirements.
 [45CSR§30-2.39]

2.12. Reasonably Anticipated Operating Scenarios

- 2.12.1. The following are terms and conditions for reasonably anticipated operating scenarios identified in this permit.
 - a. Contemporaneously with making a change from one operating scenario to another, the permittee shall record in a log at the permitted facility a record of the scenario under which it is operating and to document the change in reports submitted pursuant to the terms of this permit and 45CSR30.
 - b. The permit shield shall extend to all terms and conditions under each such operating scenario; and
 - c. The terms and conditions of each such alternative scenario shall meet all applicable requirements and the requirements of 45CSR30.

[45CSR§30-5.1.i.]

2.13. Duty to Comply

2.13.1. The permittee must comply with all conditions of this permit. Any permit noncompliance constitutes a violation of the West Virginia Code and the Clean Air Act and is grounds for enforcement action by the Secretary or USEPA; for permit termination, revocation and reissuance, or modification; or for denial of a permit renewal application. [45CSR§30-5.1.f.1.]

2.14. Inspection and Entry

- 2.14.1. The permittee shall allow any authorized representative of the Secretary, upon the presentation of credentials and other documents as may be required by law, to perform the following:
 - a. At all reasonable times (including all times in which the facility is in operation) enter upon the permittee's premises where a source is located or emissions related activity is conducted, or where records must be kept under the conditions of this permit;
 - b. Have access to and copy, at reasonable times, any records that must be kept under the conditions of this permit;
 - c. Inspect at reasonable times (including all times in which the facility is in operation) any facilities, equipment (including monitoring and air pollution control equipment), practices, or operations regulated or required under the permit;
 - d. Sample or monitor at reasonable times substances or parameters to determine compliance with the permit or applicable requirements or ascertain the amounts and types of air pollutants discharged.

[45CSR§30-5.3.b.]

2.15. Schedule of Compliance

- 2.15.1. For sources subject to a compliance schedule, certified progress reports shall be submitted consistent with the applicable schedule of compliance set forth in this permit and 45CSR§30-4.3.h., but at least every six (6) months, and no greater than once a month, and shall include the following:
 - a. Dates for achieving the activities, milestones, or compliance required in the schedule of compliance, and dates when such activities, milestones or compliance were achieved; and
 - b. An explanation of why any dates in the schedule of compliance were not or will not be met, and any preventative or corrective measure adopted.
 [45CSR§30-5.3.d.]

2.16. Need to Halt or Reduce Activity not a Defense

2.16.1. It shall not be a defense for a permittee in an enforcement action that it would have been necessary to halt or reduce the permitted activity in order to maintain compliance with the conditions of this permit. However, nothing in this paragraph shall be construed as precluding consideration of a need to halt or reduce activity as a mitigating factor in determining penalties for noncompliance if the health, safety, or environmental impacts of halting or reducing operations would be more serious than the impacts of continued operations. [45CSR§30-5.1.f.2.]

2.17. Emergency

- 2.17.1. An "emergency" means any situation arising from sudden and reasonably unforeseeable events beyond the control of the source, including acts of God, which situation requires immediate corrective action to restore normal operation, and that causes the source to exceed a technology-based emission limitation under the permit, due to unavoidable increases in emissions attributable to the emergency. An emergency shall not include noncompliance to the extent caused by improperly designed equipment, lack of preventative maintenance, careless or improper operation, or operator error. [45CSR§30-5.7.a.]
- 2.17.2. Effect of any emergency. An emergency constitutes an affirmative defense to an action brought for noncompliance with such technology-based emission limitations if the conditions of 45CSR§30-5.7.c. are met.
 [45CSR§30-5.7.b.]
- 2.17.3. The affirmative defense of emergency shall be demonstrated through properly signed, contemporaneous operating logs, or other relevant evidence that:
 - a. An emergency occurred and that the permittee can identify the cause(s) of the emergency;
 - b. The permitted facility was at the time being properly operated;
 - c. During the period of the emergency the permittee took all reasonable steps to minimize levels of emissions that exceeded the emission standards, or other requirements in the permit; and
 - d. Subject to the requirements of 45CSR§30-5.1.c.3.C.1, the permittee submitted notice of the emergency to the Secretary within one (1) working day of the time when emission limitations were exceeded due to

the emergency and made a request for variance, and as applicable rules provide. This notice, report, and variance request fulfills the requirement of 45CSR§30-5.1.c.3.B. This notice must contain a detailed description of the emergency, any steps taken to mitigate emissions, and corrective actions taken.

[45CSR§30-5.7.c.]

- 2.17.4. In any enforcement proceeding, the permittee seeking to establish the occurrence of an emergency has the burden of proof.
 [45CSR§30-5.7.d.]
- 2.17.5. This provision is in addition to any emergency or upset provision contained in any applicable requirement. [45CSR\$30-5.7.e.]

2.18. Federally-Enforceable Requirements

- 2.18.1. All terms and conditions in this permit, including any provisions designed to limit a source's potential to emit and excepting those provisions that are specifically designated in the permit as "State-enforceable only", are enforceable by the Secretary, USEPA, and citizens under the Clean Air Act. [45CSR§30-5.2.a.]
- 2.18.2. Those provisions specifically designated in the permit as "State-enforceable only" shall become "Federallyenforceable" requirements upon SIP approval by the USEPA.

2.19. Duty to Provide Information

2.19.1. The permittee shall furnish to the Secretary within a reasonable time any information the Secretary may request in writing to determine whether cause exists for modifying, revoking and reissuing, or terminating the permit or to determine compliance with the permit. Upon request, the permittee shall also furnish to the Secretary copies of records required to be kept by the permittee. For information claimed to be confidential, the permittee shall furnish such records to the Secretary along with a claim of confidentiality in accordance with 45CSR31. If confidential information is to be sent to USEPA, the permittee shall directly provide such information to USEPA along with a claim of confidentiality in accordance with 40 C.F.R. Part 2. [45CSR§30-5.1.f.5.]

2.20. Duty to Supplement and Correct Information

2.20.1. Upon becoming aware of a failure to submit any relevant facts or a submittal of incorrect information in any permit application, the permittee shall promptly submit to the Secretary such supplemental facts or corrected information.
 [45CSR§30-4.2.]

2.21. Permit Shield

2.21.1. Compliance with the conditions of this permit shall be deemed compliance with any applicable requirements as of the date of permit issuance provided that such applicable requirements are included and are specifically identified in this permit or the Secretary has determined that other requirements specifically identified are not applicable to the source and this permit includes such a determination or a concise summary thereof. [45CSR§30-5.6.a.]

- 2.21.2. Nothing in this permit shall alter or affect the following:
 - a. The liability of an owner or operator of a source for any violation of applicable requirements prior to or at the time of permit issuance; or
 - b. The applicable requirements of the Code of West Virginia and Title IV of the Clean Air Act (Acid Deposition Control), consistent with § 408 (a) of the Clean Air Act.
 - c. The authority of the Administrator of U.S. EPA to require information under § 114 of the Clean Air Act or to issue emergency orders under § 303 of the Clean Air Act.

[45CSR§30-5.6.c.]

2.22. Credible Evidence

2.22.1. Nothing in this permit shall alter or affect the ability of any person to establish compliance with, or a violation of, any applicable requirement through the use of credible evidence to the extent authorized by law. Nothing in this permit shall be construed to waive any defenses otherwise available to the permittee including but not limited to any challenge to the credible evidence rule in the context of any future proceeding. [45CSR\$30-5.3.e.3.B. and 45CSR38]

2.23. Severability

2.23.1. The provisions of this permit are severable. If any provision of this permit, or the application of any provision of this permit to any circumstance is held invalid by a court of competent jurisdiction, the remaining permit terms and conditions or their application to other circumstances shall remain in full force and effect. [45CSR§30-5.1.e.]

2.24. Property Rights

2.24.1. This permit does not convey any property rights of any sort or any exclusive privilege. [45CSR\$30-5.1.f.4]

2.25. Acid Deposition Control

- 2.25.1. Emissions shall not exceed any allowances that the source lawfully holds under Title IV of the Clean Air Act (Acid Deposition Control) or rules of the Secretary promulgated thereunder.
 - a. No permit revision shall be required for increases in emissions that are authorized by allowances acquired pursuant to the acid deposition control program, provided that such increases do not require a permit revision under any other applicable requirement.
 - b. No limit shall be placed on the number of allowances held by the source. The source may not, however, use allowances as a defense to noncompliance with any other applicable requirement.
 - c. Any such allowance shall be accounted for according to the procedures established in rules promulgated under Title IV of the Clean Air Act.

[45CSR§30-5.1.d.]

2.25.2. Where applicable requirements of the Clean Air Act are more stringent than any applicable requirement of regulations promulgated under Title IV of the Clean Air Act (Acid Deposition Control), both provisions shall be incorporated into the permit and shall be enforceable by the Secretary and U. S. EPA. [45CSR\$30-5.1.a.2.]

3.0 Facility-Wide Requirements

3.1. Limitations and Standards

- 3.1.1. **Open burning.** The open burning of refuse by any person is prohibited except as noted in 45CSR§6-3.1. [45CSR§6-3.1.]
- 3.1.2. Open burning exemptions. The exemptions listed in 45CSR§6-3.1 are subject to the following stipulation: Upon notification by the Secretary, no person shall cause or allow any form of open burning during existing or predicted periods of atmospheric stagnation. Notification shall be made by such means as the Secretary may deem necessary and feasible. [45CSR§6-3.2.]
- 3.1.3. Asbestos. The permittee is responsible for thoroughly inspecting the facility, or part of the facility, prior to commencement of demolition or renovation for the presence of asbestos and complying with 40 C.F.R. § 61.145, 40 C.F.R. § 61.148, and 40 C.F.R. § 61.150. The permittee, owner, or operator must notify the Secretary at least ten (10) working days prior to the commencement of any asbestos removal on the forms prescribed by the Secretary if the permittee is subject to the notification requirements of 40 C.F.R. § 61.145(b)(3)(i). The USEPA, the Division of Waste Management and the Bureau for Public Health Environmental Health require a copy of this notice to be sent to them.
 [40 C.F.R. §61.145(b) and 45CSR34]
- 3.1.4. Odor. No person shall cause, suffer, allow or permit the discharge of air pollutants which cause or contribute to an objectionable odor at any location occupied by the public.
 [45CSR§4-3.1 State-Enforceable only.]
- 3.1.5. Standby plan for reducing emissions. When requested by the Secretary, the permittee shall prepare standby plans for reducing the emissions of air pollutants in accordance with the objectives set forth in Tables I, II, and III of 45CSR11.
 [45CSR\$11-5.2]
- 3.1.6. Emission inventory. The permittee is responsible for submitting, on an annual basis, an emission inventory in accordance with the submittal requirements of the Division of Air Quality.
 [W.Va. Code § 22-5-4(a)(14)]
- 3.1.7. Ozone-depleting substances. For those facilities performing maintenance, service, repair or disposal of appliances, the permittee shall comply with the standards for recycling and emissions reduction pursuant to 40 C.F.R. Part 82, Subpart F, except as provided for Motor Vehicle Air Conditioners (MVACs) in Subpart B:
 - a. Persons opening appliances for maintenance, service, repair, or disposal must comply with the prohibitions and required practices pursuant to 40 C.F.R. §§ 82.154 and 82.156.
 - b. Equipment used during the maintenance, service, repair, or disposal of appliances must comply with the standards for recycling and recovery equipment pursuant to 40 C.F.R. § 82.158.

Page 13 of 49

c. Persons performing maintenance, service, repair, or disposal of appliances must be certified by an approved technician certification program pursuant to 40 C.F.R. § 82.161.

[40 C.F.R. 82, Subpart F]

- 3.1.8. Risk Management Plan. Should this stationary source, as defined in 40 C.F.R. § 68.3, become subject to Part 68, then the owner or operator shall submit a risk management plan (RMP) by the date specified in 40 C.F.R. § 68.10 and shall certify compliance with the requirements of Part 68 as part of the annual compliance certification as required by 40 C.F.R. Part 70 or 71.
 [40 C.F.R. 68]
- 3.1.9. Only those emission units/sources as identified in Table 1.1, with the exception of any *de minimis* sources as identified under Table 45-13B of 45CSR13, are authorized at the permitted facility by this permit. In accordance with the information filed in Permit application-R13-1856A, the emission units/sources identified under Table 1.1 of this permit shall be installed, maintained, and operated so as to minimize any fugitive escape of pollutants, shall not exceed the listed maximum design capacities, shall use the specified control devices, and comply with any other information provided under Table 1.1.
 [45CSR13, R13-1856, Condition 4.1.1]
- 3.1.10. Facilities using Mercaptan Tanks shall use proper odor control methods to comply with 45CSR4. [45CSR\$30-12.7 State-Enforceable only.]
- 3.1.11. Emergency Operating Condition/Unit Replacement:

For emergency situations which interrupt the critical supply of natural gas to the public, and which pose a life threatening circumstance to the customer, the permittee is allowed to temporarily replace failed engine(s) as long as all of the following conditions are met:

- a. The replacement engine(s) is only allowed to operate until repair of the failed engine(s) is complete, but under no circumstance may the replacement engine(s) operate in excess of sixty (60) days;
- b. Both the replacement engine(s) and the repaired failed engine(s) shall not operate at the same time with the exception of any necessary testing of the repaired engine(s) and this testing may not exceed five (5) hours;
- c. Potential hourly emissions from the replacement engine(s) are less than or equal to the potential hourly emissions from the engine(s) being replaced;
- d. Credible performance emission test data verifying the emission rates associated with the operation of the substitute engine shall be submitted to the Director within five (5) business days;
- e. The permittee must provide written notification to the Director within five (5) business days of the replacement. This notification must contain:
 - i. Information to support the claim of life threatening circumstances to justify applicability of this emergency provision;
 - ii. Identification of the engine(s) being temporarily replaced;

- iii. The design parameters of the replacement engine(s) including, but not limited to, the design horsepower and emission factors;
- iv. Projected duration of the replacement engine(s); and

v. The appropriate certification by a responsible official. **[45CSR§30-12.7]**

3.1.12. 40 C.F.R. 60, Subpart OOOOa

For each affected facility under §60.5365a(j), you must reduce VOC emissions by complying with the requirements of paragraphs (a) through (j) of §60.5397a. The requirements in this section are independent of the closed vent system and cover requirements in §60.5411a.

- a. You must monitor all fugitive emission components, as defined in §60.5430a, in accordance with 40 C.F.R. §§60.5397a(b) through (g). You must repair all sources of fugitive emissions in accordance with 40 C.F.R. §60.5397a(h). You must keep records in accordance with 40 C.F.R. §60.5397a(i) and report in accordance with 40 C.F.R. §60.5397a(j). For purposes of this section, fugitive emissions are defined as any visible emission from a fugitive emissions component observed using optical gas imaging or an instrument reading of 500 parts per million (ppm) or greater using Method 21 of appendix A-7 of 40 CFR part 60.
- b. You must develop an emissions monitoring plan that covers the collection of fugitive emissions components at well sites and compressor stations within each company-defined area in accordance with 40 C.F.R. §§60.5397a(c) and (d).
- c. Fugitive emissions monitoring plans must include the elements specified in 40 C.F.R. §§60.5397a(c)(1) through (8), at a minimum.
 - 1. Frequency for conducting surveys. Surveys must be conducted at least as frequently as required by 40 C.F.R. §§60.5397a(f) and (g).
 - 2. Technique for determining fugitive emissions (i.e., Method 21 at 40 CFR part 60, appendix A-7, or optical gas imaging meeting the requirements in 40 CFR §60.5397a paragraphs (c)(7)(i) through (vii)).
 - 3. Manufacturer and model number of fugitive emissions detection equipment to be used.
 - 4. Procedures and timeframes for identifying and repairing fugitive emissions components from which fugitive emissions are detected, including timeframes for fugitive emission components that are unsafe to repair. Your repair schedule must meet the requirements of 40 C.F.R. §60.5397a(h) at a minimum.
 - 5. Procedures and timeframes for verifying fugitive emission component repairs.
 - 6. Records that will be kept and the length of time records will be kept.
 - 7. If you are using optical gas imaging, your plan must also include the elements specified in 40 C.F.R. §§60.5397a(c)(7)(i) through (vii).

- i. Verification that your optical gas imaging equipment meets the specifications of 40 C.F.R. §§60.5397a(c)(7)(i)(A) and (B). This verification is an initial verification and may either be performed by the facility, by the manufacturer, or by a third party. For the purposes of complying with the fugitive emissions monitoring program with optical gas imaging, a fugitive emission is defined as any visible emissions observed using optical gas imaging.
 - A. Your optical gas imaging equipment must be capable of imaging gases in the spectral range for the compound of highest concentration in the potential fugitive emissions.
 - B. Your optical gas imaging equipment must be capable of imaging a gas that is half methane, half propane at a concentration of 10,000 ppm at a flow rate of ≤ 60 g/hr from a quarter inch diameter orifice.
- ii. Procedure for a daily verification check.
- iii. Procedure for determining the operator's maximum viewing distance from the equipment and how the operator will ensure that this distance is maintained.
- iv. Procedure for determining maximum wind speed during which monitoring can be performed and how the operator will ensure monitoring occurs only at wind speeds below this threshold.
- v. Procedures for conducting surveys, including the items specified in 40 C.F.R. \$\$60.5397a(c)(7)(v)(A) through (C).
 - A. How the operator will ensure an adequate thermal background is present in order to view potential fugitive emissions.
 - B. How the operator will deal with adverse monitoring conditions, such as wind.
 - C. How the operator will deal with interferences (e.g., steam).
- vi. Training and experience needed prior to performing surveys.
- vii. Procedures for calibration and maintenance. At a minimum, procedures must comply with those recommended by the manufacturer.
- 8. If you are using Method 21 of appendix A-7 of this part, your plan must also include the elements specified in 40 C.F.R. §§60.5397a(c)(8)(i) through (iii). For the purposes of complying with the fugitive emissions monitoring program using Method 21 of appendix A-7 of 40 CFR part 60 a fugitive emission is defined as an instrument reading of 500 ppm or greater.
 - i. Verification that your monitoring equipment meets the requirements specified in Section 6.0 of Method 21 at 40 CFR part 60, appendix A-7. For purposes of instrument capability, the fugitive emissions definition shall be 500 ppm or greater methane using a FID-based instrument. If you wish to use an analyzer other than a FID-based instrument, you must develop a site-specific fugitive emission definition that would be equivalent to 500 ppm methane using a FID-based instrument (e.g., 10.6 eV PID with a specified isobutylene concentration as the fugitive emission definition would provide equivalent response to your compound of interest).

- ii. Procedures for conducting surveys. At a minimum, the procedures shall ensure that the surveys comply with the relevant sections of Method 21 at 40 CFR part 60, appendix A-7, including Section 8.3.1.
- iii. Procedures for calibration. The instrument must be calibrated before use each day of its use by the procedures specified in Method 21 of appendix A-7 of this part. At a minimum, you must also conduct precision tests at the interval specified in Method 21 of appendix A-7 of this part, Section 8.1.2, and a calibration drift assessment at the end of each monitoring day. The calibration drift assessment must be conducted as specified in paragraph (c)(8)(iii)(A) of 40 C.F.R. §60.5397a. Corrective action for drift assessments is specified in paragraphs (c)(8)(iii)(B) and (C) of 40 C.F.R. §60.5397.
 - a. Check the instrument using the same calibration gas that was used to calibrate the instrument before use. Follow the procedures specified in Method 21 of appendix A-7 of 40 CFR part 60, Section 10.1, except do not adjust the meter readout to correspond to the calibration gas value. If multiple scales are used, record the instrument reading for each scale used. Divide the arithmetic difference of the initial and post-test calibration response by the corresponding calibration gas value for each scale and multiply by 100 to express the calibration drift as a percentage.
 - b. If a calibration drift assessment shows a negative drift of more than 10 percent, then all equipment with instrument readings between the fugitive emission definition multiplied by (100 minus the percent of negative drift/divided by 100) and the fugitive emission definition that was monitored since the last calibration must be re-monitored.
 - c. If any calibration drift assessment shows a positive drift of more than 10 percent from the initial calibration value, then, at the owner/operator's discretion, all equipment with instrument readings above the fugitive emission definition and below the fugitive emission definition multiplied by (100 plus the percent of positive drift/divided by 100) monitored since the last calibration may be re-monitored.
- d. Each fugitive emissions monitoring plan must include the elements specified in 40 C.F.R. §§60.5397a(d)(1) through (3), at a minimum, as applicable.
 - 1. If you are using optical gas imaging, your plan must include procedures to ensure that all fugitive emissions components are monitored during each survey. Example procedures include, but are not limited to, a sitemap with an observation path, a written narrative of where the fugitive emissions components are located and how they will be monitored, or an inventory of fugitive emissions components.
 - 2. If you are using Method 21 of appendix A-7 of 40 CFR part 60, your plan must include a list of fugitive emissions components to be monitored and method for determining the location of fugitive emissions components to be monitored in the field (e.g., tagging, identification on a process and instrumentation diagram, etc.).
 - 3. Your fugitive emissions monitoring plan must include the written plan developed for all of the fugitive emissions components designated as difficult-to-monitor in accordance with 40 C.F.R. §60.5397a(g)(3), and the written plan for fugitive emissions components designated as unsafe-to-monitor in accordance with 40 C.F.R. §60.5397a(g).

- e. Each monitoring survey shall observe each fugitive emissions component, as defined in §60.5430a, for fugitive emissions.
- f. 1. You must conduct an initial monitoring survey within 90 days of the startup of production, as defined in §60.5430a, for each collection of fugitive emissions components at a new well site or by June 3, 2017, whichever is later. For a modified collection of fugitive emissions components at a well site, the initial monitoring survey must be conducted within 90 days of the startup of production for each collection of fugitive emission components after the modification or by June 3, 2017, whichever is latest.
 - 2. You must conduct an initial monitoring survey within 90 days of the startup of a new compressor station for each collection of fugitive emissions components at the new compressor station or by June 3, 2017, whichever is later. For a modified collection of fugitive emissions components at a compressor station, the initial monitoring survey must be conducted within 90 days of the modification or by June 3, 2017, whichever is later.
- g. A monitoring survey of each collection of fugitive emissions components at a well site or at a compressor station must be performed at the frequencies specified in 40 C.F.R. §§60.5397a(g)(1) and (2), with the exceptions noted in 40 C.F.R. §§60.5397a(g)(3) through (5).
 - 1. A monitoring survey of each collection of fugitive emissions components at a well site within a company-defined area must be conducted at least semiannually after the initial survey. Consecutive semiannual monitoring surveys must be conducted at least 4 months apart and no more than 7 months apart.
 - 2. A monitoring survey of the collection of fugitive emissions components at a compressor station must be conducted at least semiannually after the initial survey. Consecutive semiannual monitoring surveys must be conducted at least 4 months apart and no more than 7 months apart.
 - 3. Fugitive emissions components that cannot be monitored without elevating the monitoring personnel more than 2 meters above the surface may be designated as difficult-to-monitor. Fugitive emissions components that are designated difficult-to-monitor must meet the specifications of 40 C.F.R. §§60.5397a(g)(3)(i) through (iv).
 - i. A written plan must be developed for all of the fugitive emissions components designated difficult-to-monitor. This written plan must be incorporated into the fugitive emissions monitoring plan required by 40 C.F.R. §§60.5397a(b), (c), and (d).
 - ii. The plan must include the identification and location of each fugitive emissions component designated as difficult-to-monitor.
 - iii. The plan must include an explanation of why each fugitive emissions component designated as difficult-to-monitor is difficult-to-monitor.
 - iv. The plan must include a schedule for monitoring the difficult-to-monitor fugitive emissions components at least once per calendar year.
 - 4. Fugitive emissions components that cannot be monitored because monitoring personnel would be exposed to immediate danger while conducting a monitoring survey may be designated as unsafe-

to-monitor. Fugitive emissions components that are designated unsafe-to-monitor must meet the specifications of 40 C.F.R. \$60.5397a(g)(4)(i) through (iv).

- i. A written plan must be developed for all of the fugitive emissions components designated unsafe-to-monitor. This written plan must be incorporated into the fugitive emissions monitoring plan required by 40 C.F.R. §§60.5397a(b), (c), and (d).
- ii. The plan must include the identification and location of each fugitive emissions component designated as unsafe-to-monitor.
- iii. The plan must include an explanation of why each fugitive emissions component designated as unsafe-to-monitor is unsafe-to-monitor.
- iv. The plan must include a schedule for monitoring the fugitive emissions components designated as unsafe-to-monitor.
- 5. You are no longer required to comply with the requirements of 40 C.F.R. §60.5397a(g)(1) when the owner or operator removes all major production and processing equipment, as defined in § 60.5430a, such that the well site becomes a wellhead only well site. If any major production and processing equipment is subsequently added to the well site, then the owner or operator must comply with the requirements in paragraphs (f)(1) and (g)(1) of 40 C.F.R. §60.5397a.
- h. Each identified source of fugitive emissions shall be repaired, as defined in 40 C.F.R. §60.5430a, in accordance with 40 C.F.R. §§60.5397a(h)(1) and (2).
 - 1. A first attempt at repair shall be made no later than 30 calendar days after the detection of the fugitive emissions.
 - 2. Repair shall be completed as soon as practicable, but no later than 30 calendar days after the first attempt at repair as required in 40 C.F.R. §60.5397a(h)(1).
 - 3. If the repair is technically infeasible, would require a vent blowdown, a compressor station shutdown, a well shutdown or well shut-in, or would be unsafe to repair during operation of the unit, the repair must be completed during the next compressor station shut down for maintenance, scheduled well shutdown, scheduled well shut-in, after a scheduled vent blowdown or within 2 years, whichever is earliest. For purposes of this condition, a vent blowdown is the opening of one or more blowdown valves to depressurize major production and processing equipment, other than a storage vessel.
 - 4. Each identified source of fugitive emissions must be resurveyed to complete repair according to 40 C.F.R. §60.5397a(h)(i) through (iv) to ensure that there are no fugitive emissions.
 - i. The operator may resurvey the fugitive emissions components to verify repair using either Method 21 of appendix A-7 of 40 CFR part 60 or optical gas imaging.
 - ii. For each repair that cannot be made during the monitoring survey when the fugitive emissions are initially found, a digital photograph must be taken of that component or the component must be tagged during the monitoring survey when the fugitives were initially found for identification purposes and subsequent repair. The digital photograph must include the date that the photograph was taken and must clearly identify the component by location within the site (e.g.,

Page 20 of 49

the latitude and longitude of the component or by other descriptive landmarks visible in the picture).

- iii. Operators that use Method 21 of appendix A-7 of 40 CFR part 60 to resurvey the repaired fugitive emissions components are subject to the resurvey provisions specified in 40 C.F.R. §§60.5397a(h)(4)(iii)(A) and (B).
 - A. A fugitive emissions component is repaired when the Method 21 instrument indicates a concentration of less than 500 ppm above background or when no soap bubbles are observed when the alternative screening procedures specified in section 8.3.3 of Method 21 of appendix A-7 of 40 CFR part 60 are used.
 - B. Operators must use the Method 21 monitoring requirements specified in 40 C.F.R. §60.5397a(c)(8)(ii) or the alternative screening procedures specified in section 8.3.3 of Method 21 of appendix A-7 of 40 CFR part 60.
- iv. Operators that use optical gas imaging to resurvey the repaired fugitive emissions components, are subject to the resurvey provisions specified in 40 C.F.R. §§60.5397a(h)(4)(iv)(A) and (B).
 - A. A fugitive emissions component is repaired when the optical gas imaging instrument shows no indication of visible emissions.
 - B. Operators must use the optical gas imaging monitoring requirements specified in 40 C.F.R. §60.5397a(c)(7).
- i. Records for each monitoring survey shall be maintained as specified §60.5420a(c)(15).
- j. Annual reports shall be submitted for each collection of fugitive emissions components at a well site and each collection of fugitive emissions components at a compressor station that include the information specified in §60.5420a(b)(7). Multiple collection of fugitive emissions components at a well site or at a compressor station may be included in a single annual report.

[45CSR13, R13-1856, Condition 4.1.5; 45CSR16; 40 C.F.R. §60.5397a]

3.1.13. No person shall cause, suffer, allow or permit fugitive particulate matter to be discharged beyond the boundary lines of the property on which the discharge originates or at any public or residential location, which causes or contributes to statutory air pollution.

When a person is found in violation of this rule, the Director may require the person to utilize a system to minimize fugitive particulate matter. This system to minimize fugitive particulate matter may include, but is not limited to, the following:

- a. Use, where practicable, of water or chemicals for control of particulate matter in demolition of existing buildings or structures, construction operations, grading of roads or the clearing of land;
- b. Application of asphalt, water or suitable chemicals on unpaved roads, material stockpiles and other surfaces which can create airborne particulate matter;
- c. Covering of material transport vehicles, or treatment of cargo, to prevent contents from dripping, sifting, leaking or otherwise escaping and becoming airborne, and prompt removal of tracked material from roads or streets; or

d. Installation and use of hoods, fans and fabric filters to enclose and vent the handling of materials, including adequate containment methods during sandblasting, abrasive cleaning or other similar operations.

[45CSR§17-3. State-Enforceable only.]

3.2. Monitoring Requirements

3.2.1. Emission Limit Averaging Time. Unless otherwise specified, compliance with all annual limits shall be based on a rolling twelve month total. A rolling twelve month total shall be the sum of the measured parameter of the previous twelve calendar months.
 [45CSR13, R13-1856, Condition 3.2.1]

3.3. Testing Requirements

- 3.3.1. **Stack testing.** As per provisions set forth in this permit or as otherwise required by the Secretary, in accordance with the West Virginia Code, underlying regulations, permits and orders, the permittee shall conduct test(s) to determine compliance with the emission limitations set forth in this permit and/or established or set forth in underlying documents. The Secretary, or his duly authorized representative, may at his option witness or conduct such test(s). Should the Secretary exercise his option to conduct such test(s), the operator shall provide all necessary sampling connections and sampling ports to be located in such manner as the Secretary may require, power for test equipment and the required safety equipment, such as scaffolding, railings and ladders, to comply with generally accepted good safety practices. Such tests shall be conducted in accordance with the methods and procedures set forth in this permit or as otherwise approved or specified by the Secretary in accordance with the following:
 - a. The Secretary may on a source-specific basis approve or specify additional testing or alternative testing to the test methods specified in the permit for demonstrating compliance with 40 C.F.R. Parts 60, 61, and 63, if applicable, in accordance with the Secretary's delegated authority and any established equivalency determination methods which are applicable.
 - b. The Secretary may on a source-specific basis approve or specify additional testing or alternative testing to the test methods specified in the permit for demonstrating compliance with applicable requirements which do not involve federal delegation. In specifying or approving such alternative testing to the test methods, the Secretary, to the extent possible, shall utilize the same equivalency criteria as would be used in approving such changes under Section 3.3.1.a. of this permit.
 - c. All periodic tests to determine mass emission limits from or air pollutant concentrations in discharge stacks and such other tests as specified in this permit shall be conducted in accordance with an approved test protocol. Unless previously approved, such protocols shall be submitted to the Secretary in writing at least thirty (30) days prior to any testing and shall contain the information set forth by the Secretary. In addition, the permittee shall notify the Secretary at least fifteen (15) days prior to any testing so the Secretary may have the opportunity to observe such tests. This notification shall include the actual date and time during which the test will be conducted and, if appropriate, verification that the tests will fully conform to a referenced protocol previously approved by the Secretary.
 - d. The permittee shall submit a report of the results of the stack test within 60 days of completion of the test. The test report shall provide the information necessary to document the objectives of the test and to determine whether proper procedures were used to accomplish these objectives. The report shall

include the following: the certification described in paragraph 3.5.1; a statement of compliance status, also signed by a responsible official; and, a summary of conditions which form the basis for the compliance status evaluation. The summary of conditions shall include the following:

- 1. The permit or rule evaluated, with the citation number and language.
- 2. The result of the test for each permit or rule condition.
- 3. A statement of compliance or non-compliance with each permit or rule condition.

[WV Code §§ 22-5-4(a)(14-15) and 45CSR13]

3.4. Recordkeeping Requirements

- 3.4.1. **Monitoring information.** The permittee shall keep records of monitoring information that include the following:
 - a. The date, place as defined in this permit and time of sampling or measurements;
 - b. The date(s) analyses were performed;
 - c. The company or entity that performed the analyses;
 - d. The analytical techniques or methods used;
 - e. The results of the analyses; and
 - f. The operating conditions existing at the time of sampling or measurement.

[45CSR13, R13-1856 Condition 4.4.1; 45CSR§30-5.1.c.2.A.]

- 3.4.2. Retention of records. The permittee shall retain records of all required monitoring data and support information for a period of at least five (5) years from the date of monitoring sample, measurement, report, application, or record creation date. Support information includes all calibration and maintenance records and all original strip-chart recordings for continuous monitoring instrumentation, and copies of all reports required by the permit. Where appropriate, records may be maintained in computerized form in lieu of the above records.
 [45CSR§30-5.1.c.2.B.]
- 3.4.3. Odors. For the purposes of 45CSR4, the permittee shall maintain a record of all odor complaints received, any investigation performed in response to such a complaint, and any responsive action(s) taken. [45CSR\$30-5.1.c. State-Enforceable only.]

3.5. Reporting Requirements

3.5.1. Responsible official. Any application form, report, or compliance certification required by this permit to be submitted to the DAQ and/or USEPA shall contain a certification by the responsible official that states that, based on information and belief formed after reasonable inquiry, the statements and information in the document are true, accurate and complete. [45CSR§§30-4.4. and 5.1.c.3.D.]

- 3.5.2. A permittee may request confidential treatment for the submission of reporting required under 45CSR§30-5.1.c.3. pursuant to the limitations and procedures of W.Va. Code § 22-5-10 and 45CSR31.
 [45CSR§30-5.1.c.3.E.]
- 3.5.3. Except for the electronic submittal of the annual compliance certification and semi-annual monitoring reports to the DAQ and USEPA as required in 3.5.5 and 3.5.6 below, all notices, requests, demands, submissions and other communications required or permitted to be made to the Secretary of DEP and/or USEPA shall be made in writing and shall be deemed to have been duly given when delivered by hand, mailed first class or by private carrier with postage prepaid to the address(es), or submitted in electronic format by e-mail as set forth below or to such other person or address as the Secretary of the Department of Environmental Protection may designate:

DAQ:

US EPA:

Director	Section Chief		
WVDEP	U.S. Environmental Protection Agency,		
Division of Air Quality	Region III Enforcement and Compliance		
601 57 th Street SE	Assurance Division Air Section (3ED21)		
Charleston, WV 25304	1650 Arch Street		
	Philadelphia, PA 19103-2029		

DAQ Compliance and Enforcement¹:

DEPAirQualityReports@wv.gov

¹For all self-monitoring reports (MACT, GACT, NSPS, etc.), stack tests and protocols, Notice of Compliance Status reports, Initial Notifications, etc.

- 3.5.4. Certified emissions statement. The permittee shall submit a certified emissions statement and pay fees on an annual basis in accordance with the submittal requirements of the Division of Air Quality. [45CSR\$30-8.]
- 3.5.5. **Compliance certification.** The permittee shall certify compliance with the conditions of this permit on the forms provided by the DAQ. In addition to the annual compliance certification, the permittee may be required to submit certifications more frequently under an applicable requirement of this permit. The annual certification shall be submitted to the DAQ and USEPA on or before March 15 of each year and shall certify compliance for the period ending December 31. The permittee shall maintain a copy of the certification on site for five (5) years from submittal of the certification. The annual certification shall be submitted in electronic format by e-mail to the following addresses:

DAQ:

DEPAirQualityReports@wv.gov

US EPA:

orts@wv.gov

R3_APD_Permits@epa.gov

[45CSR§30-5.3.e.]

3.5.6. **Semi-annual monitoring reports.** The permittee shall submit reports of any required monitoring on or before September 15 for the reporting period January 1 to June 30 and on or before March 15 for the reporting period July 1 to December 31. All instances of deviation from permit requirements must be clearly identified in such reports. All required reports must be certified by a responsible official consistent with 45CSR§30-4.4. The semi-annual monitoring reports shall be submitted in electronic format by e-mail to the following address:

DAQ:

DEPAirQualityReports@wv.gov

[45CSR§30-5.1.c.3.A.]

3.5.7. Emergencies. For reporting emergency situations, refer to Section 2.17 of this permit.

3.5.8. **Deviations.**

- a. In addition to monitoring reports required by this permit, the permittee shall promptly submit supplemental reports and notices in accordance with the following:
 - 1. Any deviation resulting from an emergency or upset condition, as defined in 45CSR§30-5.7., shall be reported by telephone or telefax within one (1) working day of the date on which the permittee becomes aware of the deviation, if the permittee desires to assert the affirmative defense in accordance with 45CSR§30-5.7. A written report of such deviation, which shall include the probable cause of such deviations, and any corrective actions or preventative measures taken, shall be submitted and certified by a responsible official within ten (10) days of the deviation.
 - 2. Any deviation that poses an imminent and substantial danger to public health, safety, or the environment shall be reported to the Secretary immediately by telephone or telefax. A written report of such deviation, which shall include the probable cause of such deviation, and any corrective actions or preventative measures taken, shall be submitted by the responsible official within ten (10) days of the deviation.
 - 3. Deviations for which more frequent reporting is required under this permit shall be reported on the more frequent basis.
 - All reports of deviations shall identify the probable cause of the deviation and any corrective actions or preventative measures taken.
 [45CSR§30-5.1.c.3.C.]
- b. The permittee shall, in the reporting of deviations from permit requirements, including those attributable to upset conditions as defined in this permit, report the probable cause of such deviations and any corrective actions or preventive measures taken in accordance with any rules of the Secretary. [45CSR\$30-5.1.c.3.B.]

- 3.5.9. New applicable requirements. If any applicable requirement is promulgated during the term of this permit, the permittee will meet such requirements on a timely basis, or in accordance with a more detailed schedule if required by the applicable requirement.
 [45CSR§30-4.3.h.1.B.]
- 3.5.10. During compliance certification, the facility shall certify that the facility burns natural gas in all stationary equipment regulated under this permit except, when applicable, for emergency equipment (i.e. diesel generators).
 [45CSR§30-5.1.c.]

3.6. Compliance Plan

3.6.1. None.

3.7. Permit Shield

- 3.7.1. The permittee is hereby granted a permit shield in accordance with 45CSR§30-5.6. The permit shield applies provided the permittee operates in accordance with the information contained within this permit.
- 3.7.2. The following requirements specifically identified are not applicable to the source based on the determinations set forth below. The permit shield shall apply to the following requirements provided the conditions of the determinations are met.
 - a. According to 45CSR§2-11.1 the boiler and heaters are exempt from the weight emission standards and MRR (monitoring, recordkeeping and reporting) because they are less than 10 mmBtu/hr.
 - b. 45CSR10; To Prevent and Control Air Pollution from the Emission of Sulfur Oxides: 45CSR10 is not applicable to the facility boiler and heaters because they are less than 10 mmBtu/hr.
 - c. 45CSR21; To Prevent and Control Air Pollution from the Emission of Volatile Organic Compounds: All storage tanks at Ceredo station are below 40,000 gallons in capacity, hence 45CSR§21-28 is not applicable. Ceredo station is not engaged in the extraction or fractionation of natural gas, hence, 45CSR§21-29 is not applicable.
 - d. 45CSR27; To Prevent and Control the Emissions of Toxic Air Pollutants: Natural gas is included as a petroleum product and contains less than 5% benzene by weight. 45CSR§27-2.4 exempts equipment "used in the production and distribution of petroleum products providing that such equipment does not produce or contact materials containing more than 5% benzene by weight."
 - e. 40 C.F.R. 60 Subpart Dc; Standards of Performance for Steam Generating Units: The boiler and heaters at this facility are less than 10 mmBtu/hr; hence, Subpart Dc is not applicable.
 - f. 40 C.F.R. 60 Subparts K, Ka; Standards of Performance for Storage Vessels for Petroleum Liquids: All tanks at Ceredo station are below 40,000 gallons in capacity.
 - g. 40 C.F.R. 60 Subpart Kb; Standards of Performance for Volatile Organic Liquid Storage Vessels: All tanks at Ceredo station are below 75m³ in capacity.

- h. 40 C.F.R. 60 Subpart KKK; Standards of Performance for Equipment Leaks of VOC From Onshore Natural Gas Processing Plant: Ceredo station is not engaged in the extraction or fractionation of natural gas liquids from field gas, the fractionation of mixed natural gas liquids to natural gas products, or both.
- i. 40 C.F.R. 60 Subpart IIII; Standards of Performance for Stationary Compression Ignition Internal Combustion Engines: There are no compression ignition engines at this facility.
- j. 40 C.F.R 60 Subpart OOOO; Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution: Storage vessel requirements do not apply since all tanks commenced construction prior to August 23, 2011.
- k. 40 C.F.R. 63 Subpart HHH; National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities: The facility does not have a glycol dehydration unit and is therefore not subject to the requirements of this subpart.
- 1. 40 C.F.R. 63 Subpart YYYY; Turbine MACT: The Solar Titan 250 (E10) is subject to 40 C.F.R. 63 Subpart YYYY. Per 40 C.F.R. §63.6095(d), there is a stay of standards for lean premix stationary combustion turbines until EPA takes final action to require compliance with this subpart. The only requirement for the unit is the initial notification requirement of 40 C.F.R. §63.6145, which was satisfied by the preconstruction permit application.
- m. 40 C.F.R. 64 None of the emission units have any add-on controls; therefore, in accordance with 40 C.F.R § 64.2(a), CAM is not applicable to this facility.

4.1. Limitations and Standards

- 4.1.1. No person shall cause, suffer, allow or permit emission of smoke and/or particulate matter into the open air from any fuel burning unit which is greater than ten (10) percent opacity based on a six minute block average.
 [45CSR§2-3.1.]
- 4.1.2. Compliance with the visible emission requirements of 45CSR§2-3.1 (Section 4.1.1 of this permit) shall be determined in accordance with 40 C.F.R. Part 60, Appendix A, Method 9 or by using measurements from continuous opacity monitoring systems approved by the Director. The Director may require the installation, calibration, maintenance and operation of continuous opacity monitoring systems and may establish policies for the evaluation of continuous opacity monitoring results and the determination of compliance with the visible emission requirements of 45CSR§2-3.1 (Section 4.1.1 of this permit). Continuous opacity monitors shall not be required on fuel burning units which employ wet scrubbing systems for emission control. [45CSR§2-3.2.]
- 4.1.3. You must meet the work practice standard in 40 C.F.R 63 Subpart DDDDD Table 3 that applies to your boiler or process heater, for each boiler or process heater at your source, except as provided under 40 C.F.R. §63.7522.

If your unit is	You must meet the following
1. A new or existing boiler or process heater with a continuous oxygen trim system that maintains an optimum air to fuel ratio, or a heat input capacity of less than or equal to 5 million Btu per hour in any of the following subcategories: unit designed to burn gas 1; unit designed to burn gas 2 (other); or unit designed to burn light liquid, or a limited use boiler or process heater (H1, H3)	Conduct a tune-up of the boiler or process heater every 5 years as specified in §63.7540.
2. A new or existing boiler or process heater without a continuous oxygen trim system and with heat input capacity of less than 10 million Btu per hour in the unit designed to burn heavy liquid or unit designed to burn solid fuel subcategories; or a new or existing boiler or process heater with heat input capacity of less than 10 million Btu per hour, but greater than 5 million Btu per hour, in any of the following subcategories: unit designed to burn gas 1; unit designed to burn gas 2 (other); or unit designed to burn light liquid (BL3)	Conduct a tune-up of the boiler or process heater biennially as specified in §63.7540.

If your unit is	You must meet the following	
4. An existing boiler or process heater located at a major source facility, not including limited use units. (H1)	Must have a one-time energy assessment performed by a qualified energy assessor. An energy assessment completed on or after January 1, 2008, that meets or is amended to meet the energy assessment requirements in this table, satisfies the energy assessment requirement. A facility that operated under an energy management program developed according to the ENERGY STAR guidelines for energy management or compatible with ISO 50001 for at least one year between January 1, 2008 and the compliance date specified in §63.7495 that includes the affected units also satisfies the energy assessment requirement. The energy assessment must include the following with extent of the evaluation for items a. to e. appropriate for the on-site technical hours listed in §63.7575:	
	a. A visual inspection of the boiler or process heater system.	
	b. An evaluation of operating characteristics of the boiler or process heater systems, specifications of energy using systems, operating and maintenance procedures, and unusual operating constraints.	
	c. An inventory of major energy use systems consuming energy from affected boilers and process heaters and which are under the control of the boiler/process heater owner/operator.	
	d. A review of available architectural and engineering plans, facility operation and maintenance procedures and logs, and fuel usage.	
	e. A review of the facility's energy management program and provide recommendations for improvements consistent with the definition of energy management program, if identified.	
	f. A list of cost-effective energy conservation measures that are within the facility's control.	
	g. A list of the energy savings potential of the energy conservation measures identified.	
	h. A comprehensive report detailing the ways to improve efficiency, the cost of specific improvements, benefits, and the time frame for recouping those investments.	

[45CSR34; 40 C.F.R. §63.7500(a)(1), 40 C.F.R. 63 Subpart DDDDD Table 3]

4.1.4. At all times, you must operate and maintain any affected source (as defined in 40 C.F.R. §63.7490), including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions. Determination of whether such operation and maintenance procedures are being used will be based on information available to the Administrator that may include, but is not limited to, monitoring results, review of operation and maintenance procedures, review of operation and maintenance records, and inspection of the source.
[45CSR34; 40 C.F.R. §63.7500(a)(3)]

- 4.1.5. Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity of less than or equal to 5 million Btu per hour must complete a tune-up every 5 years as specified in 40 C.F.R. §63.7540. Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity greater than 5 million Btu per hour and less than 10 million Btu per hour must complete a tune-up every 2 years as specified in 40 C.F.R. §63.7540. Boilers and process heaters in the units designed to burn gas 1 fuels subcategory are not subject to the emission limits in Tables 1 and 2 or 11 through 13 of 40 C.F.R. 63 subpart DDDDD, or the operating limits in Table 4 of 40 C.F.R. 63 subpart DDDDD. [45CSR34; 40 C.F.R. §63.7500(e)]
- 4.1.6. For existing affected sources (as defined in 40 C.F.R. §63.7490), you must complete the initial compliance demonstrations, as specified in 40 C.F.R. §63.7510(a) through (d), no later than 180 days after the compliance date that is specified for your source in 40 C.F.R. §63.7495 and according to the applicable provisions in 40 C.F.R. §63.7(a)(2) as cited in 40 C.F.R. 63 Subpart DDDDD Table 10, except as specified in 40 C.F.R. §63.7510(j). You must complete an initial tune-up by following the procedures described in 40 C.F.R. §63.7540(a)(10)(i) through (vi) no later than the compliance date specified in 40 C.F.R. §63.7495, except as specified in 40 C.F.R. §63.7510(j). You must complete the one-time energy assessment specified in Table 3 to this subpart no later than the compliance date specified in 40 C.F.R. §63.7495.
 [45CSR34; 40 C.F.R. §63.7510(e)](H1)
- 4.1.7. For new or reconstructed affected sources (as defined in 40 C.F.R. §63.7490), you must demonstrate initial compliance with the applicable work practice standards in 40 C.F.R. 63 Subpart DDDDD Table 3 within the applicable annual, biennial, or 5-year schedule as specified in 40 C.F.R. §63.7515(d) following the initial compliance date specified in 40 C.F.R. §63.7495(a). Thereafter, you are required to complete the applicable annual, biennial, or 5-year tune-up as specified in 40 C.F.R. §63.7515(d).
 [45CSR34; 40 C.F.R. §63.7510(g)](H3 and BL3)
- 4.1.8. If you are required to meet an applicable tune-up work practice standard, you must conduct an annual, biennial, or 5-year performance tune-up according to 40 C.F.R. §63.7540(a)(10), (11), or (12), respectively. Each annual tune-up specified in 40 C.F.R. §63.7540(a)(10) must be no more than 13 months after the previous tune-up. Each biennial tune-up specified in 40 C.F.R. §63.7540(a)(11) must be conducted no more than 25 months after the previous tune-up. Each 5-year tune-up specified in 40 C.F.R. §63.7540(a)(12) must be conducted no more than 61 months after the previous tune-up. For a new or reconstructed affected source (as defined in 40 C.F.R. §63.7490), the first annual, biennial, or 5-year tune-up must be no later than 13 months, 25 months, or 61 months, respectively, after April 1, 2013 or the initial startup of the new or reconstructed affected source, whichever is later. [45CSR34; 40 C.F.R. §63.7515(d)]
- 4.1.9. If your boiler or process heater has a heat input capacity of less than 10 million Btu per hour (except as specified in 40 C.F.R. §63.7540(a)(12)), you must conduct a biennial tune-up of the boiler or process heater as specified in 40 C.F.R §63.7540(a)(10)(i) through (vi) to demonstrate continuous compliance. [45CSR34; 40 C.F.R. §63.7540(a)(11)](BL3)
- 4.1.10. If your boiler or process heater has a continuous oxygen trim system that maintains an optimum air to fuel ratio or a heat input capacity of less than or equal to 5 million Btu per hour and the unit is in the units designed to burn gas 1; you must conduct a tune-up of the boiler or process heater every 5 years as specified in paragraphs 40 C.F.R. §63.7540(a)(10)(i) through (vi) to demonstrate continuous compliance. You may delay the burner inspection specified in paragraph 40 C.F.R. §63.7540(a)(10)(i) until the next scheduled or unscheduled unit shutdown, but you must inspect each burner at least once every 72 months. If an oxygen

trim system is utilized on a unit without emission standards to reduce the tune-up frequency to once every 5 years, set the oxygen level no lower than the oxygen concentration measured during the most recent tune-up. These tune-ups shall consist of the following:

- a. As applicable, inspect the burner, and clean or replace any components of the burner as necessary (you may perform the burner inspection any time prior to the tune-up or delay the burner inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the burner inspection until the first outage, not to exceed 36 months from the previous inspection. At units where entry into a piece of process equipment or into a storage vessel is required to complete the tune-up inspections, inspections are required only during planned entries into the storage vessel or process equipment;
- b. Inspect the flame pattern, as applicable, and adjust the burner as necessary to optimize the flame pattern. The adjustment should be consistent with the manufacturer's specifications, if available;
- c. Inspect the system controlling the air-to-fuel ratio, as applicable, and ensure that it is correctly calibrated and functioning properly (you may delay the inspection until the next scheduled unit shutdown). Units that produce electricity for sale may delay the inspection until the first outage, not to exceed 36 months from the previous inspection;
- d. Optimize total emissions of CO. This optimization should be consistent with the manufacturer's specifications, if available, and with any NO_X requirement to which the unit is subject;
- e. Measure the concentrations in the effluent stream of CO in parts per million, by volume, and oxygen in volume percent, before and after the adjustments are made (measurements may be either on a dry or wet basis, as long as it is the same basis before and after the adjustments are made). Measurements may be taken using a portable CO analyzer; and
- f. Maintain on-site and submit, if requested by the Administrator, a report containing the following information:
 - i. The concentrations of CO in the effluent stream in parts per million by volume, and oxygen in volume percent, measured at high fire or typical operating load, before and after the tune-up of the boiler or process heater;
 - ii. A description of any corrective actions taken as a part of the tune-up; and
 - iii. The type and amount of fuel used over the 12 months prior to the tune-up, but only if the unit was physically and legally capable of using more than one type of fuel during that period. Units sharing a fuel meter may estimate the fuel used by each unit.

[45CSR34; 40 C.F.R. §§63.7540(a)(10) & (a)(12)]

- 4.1.11. The Heater, identified as H3, shall operate according to the following requirements:
 - a. The MDHI shall not exceed 0.6 mmBtu/hr and the unit shall only be fired by natural gas;
 - b. As the annual emission limits given in table 4.1.11(c) are based on operating 8,760 hours/year, there is no limit on the annual hours of operation or fuel usage of the Heater.

c. The maximum combustion exhaust emissions from the Heater shall not exceed the limits given in the following table;

Table 4.1.11.c:	Heater	Emission	Limits
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Pollutant	PPH	TPY
CO	0.05	0.22
NO _x	0.06	0.26

d. 45CSR2

No person shall cause, suffer, allow or permit emission of smoke and/or particulate matter into the open air from any fuel burning unit which is greater than ten (10) percent opacity based on a six minute block average.

[45CSR§2-3.1.]

e. 40 C.F.R. 63 Subpart DDDDD

Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity of less than or equal to 5 million Btu per hour must complete a tune-up every 5 years as specified in §63.7540. Boilers and process heaters in the units designed to burn gas 1 fuels subcategory with a heat input capacity greater than 5 million Btu per hour and less than 10 million Btu per hour must complete a tune-up every 2 years as specified in §63.7540. Boilers and process heaters in the units designed to burn gas 1 fuels subcategory are not subject to the emission limits in Tables 1 and 2 or 11 through 13 to this subpart, or the operating limits in Table 4 to this subpart. **[45CSR34, 40 C.F.R. §63.7500(e)]**

[45CSR13, R13-1856, Condition 4.1.4](H3)

4.2. Monitoring Requirements

4.2.1. At such reasonable times as the Secretary may designate, the permittee shall conduct visible emissions observations using Method 22 for the purpose of demonstrating compliance with Section 4.1.1. If visible emissions are observed, the permittee shall conduct a Method 9 reading unless the cause for visible emissions is corrected within 24 hours. Records of observation will be kept for at least 5 years from the date of observation.

[45CSR§30-5.1.c.]

4.3. Testing Requirements

4.3.1. At such reasonable times(s) as the Secretary may designate, in accordance with the provisions of 3.3.1 of this permit, the permittee shall conduct of have conducted test(s) to determine compliance with the emission limitations established in this permit and/or applicable regulations.
 [45CSR13, R13-1856, Condition 4.3.1](H3)

4.4. Recordkeeping Requirements

4.4.1. You must keep records of each notification and report that you submitted to comply with 40 C.F.R. 63 Subpart DDDDD, including all documentation supporting any Initial Notification or Notification of Compliance Status or semiannual compliance report that you submitted, according to the requirements in 40 C.F.R. §63.10(b)(2)(xiv).

[45CSR34; 40 C.F.R. §63.7555(a)(1)]

- 4.4.2. In what form and how long must I keep my records?
 - a. Your records must be in a form suitable and readily available for expeditious review, according to 40 C.F.R. §63.10(b)(1).
 - b. As specified in 40 C.F.R.§63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.
 - c. You must keep each record on site, or they must be accessible from on site (for example, through a computer network), for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to 40 C.F.R. §63.10(b)(1). You can keep the records off site for the remaining 3 years.

[45CSR34; 40 C.F.R. §63.7560]

4.5. **Reporting Requirements**

- 4.5.1. You must include with the Notification of Compliance Status a signed certification that either the energy assessment was completed according to 40 C.F.R. 63 Subpart DDDDD Table 3, and that the assessment is an accurate depiction of your facility at the time of the assessment, or that the maximum number of on-site technical hours specified in the definition of energy assessment applicable to the facility has been expended. [45CSR34; 40 C.F.R. §63.7530(e)](H1)
- 4.5.2. You must submit the Notification of Compliance Status containing the results of the initial compliance demonstration according to the requirements in40 C.F.R. §63.7545(e).
 [45CSR34; 40 C.F.R. §63.7530(f)]
- 4.5.3. If you are not required to conduct an initial compliance demonstration as specified in 40 C.F.R. §63.7530(a), the Notification of Compliance Status must only contain the information specified in 40 C.F.R. §§63.7545(e)(1) and (8) and must be submitted within 60 days of the compliance date specified at 40 C.F.R. §63.7495(b).
 - a. A description of the affected unit(s) including identification of which subcategories the unit is in, the design heat input capacity of the unit, a description of the add-on controls used on the unit to comply with this subpart, description of the fuel(s) burned, including whether the fuel(s) were a secondary material determined by you or the EPA through a petition process to be a non-waste under \$241.3 of this chapter, whether the fuel(s) were a secondary material processed from discarded non-hazardous secondary materials within the meaning of \$241.3 of this chapter, and justification for the selection of fuel(s) burned during the compliance demonstration.
 - b. In addition to the information required in 40 C.F.R. §63.9(h)(2), your notification of compliance status must include the following certification(s) of compliance, as applicable, and signed by a responsible official:
 - i. "This facility completed the required initial tune-up for all of the boilers and process heaters covered by 40 CFR part 63 subpart DDDDD at this site according to the procedures in 40 C.F.R. §63.7540(a)(10)(i) through (vi)."

- ii. "This facility has had an energy assessment performed according to §63.7530(e)."
- iii. Except for units that burn only natural gas, refinery gas, or other gas 1 fuel, or units that qualify for a statutory exemption as provided in section 129(g)(1) of the Clean Air Act, include the following: "No secondary materials that are solid waste were combusted in any affected unit."

[45CSR34; 40 C.F.R. §63.7545(e)(1) and (8)]

- 4.5.4. Unless the EPA Administrator has approved a different schedule for submission of reports under §63.10(a), you must submit each report, according to paragraph 40 C.F.R. §63.7550(h), by the date in 40 C.F.R. 63 Subpart DDDDD Table 9 and according to the requirements in 40 C.F.R. §§63.7550(b)(1) through (4). For units that are subject only to a requirement to conduct subsequent annual, biennial, or 5-year tune-up according to §63.7540(a)(10), (11), or (12), respectively, and not subject to emission limits or Table 4 operating limits, you may submit only an annual, biennial, or 5-year compliance report, as applicable, as specified in 40 C.F.R. §§63.7550(b)(1) through (4), instead of a semi-annual compliance report. [45CSR34; 40 C.F.R. §63.7550(b)]
- 4.5.5. For each affected source that is subject to permitting regulations pursuant to part 70 or part 71 of this chapter, and if the permitting authority has established dates for submitting semiannual reports pursuant to 70.6(a)(3)(iii)(A) or 71.6(a)(3)(iii)(A), you may submit the first and subsequent compliance reports according to the dates the permitting authority has established in the permit instead of according to the dates in 40 C.F.R. §§63.7550(b)(1) through (4).
 [45CSR34; 40 C.F.R. §63.7550(b)(5)]
- 4.5.6. A compliance report must contain the following information depending on how the facility chooses to comply with the limits set in this rule.
 - a. Company and Facility name and address.
 - b. Process unit information, emissions limitations, and operating parameter limitations.
 - c. Date of report and beginning and ending dates of the reporting period.
 - d. Include the date of the most recent tune-up for each unit subject to only the requirement to conduct an annual, biennial, or 5-year tune-up according to 40 C.F.R. §63.7540(a)(10), (11), or (12) respectively. Include the date of the most recent burner inspection if it was not done annually, biennially, or on a 5-year period and was delayed until the next scheduled or unscheduled unit shutdown.
 - e. Statement by a responsible official with that official's name, title, and signature, certifying the truth, accuracy, and completeness of the content of the report.

[45CSR34; 40 C.F.R. §§63.7550(c), (c)(1), (c)(5)(i)-(iii), (c)(5)(xiv), and (c)(5)(xvii)]

4.6. Compliance Plan

4.6.1. None.
5.0 Source Specific Requirements [emission point ID(s): E01, E02, E03, E04, E05, E06, E07, G3, G4]

5.1. Limitations and Standards

- 5.1.1. The following stationary RICE do not have to meet the requirements of 40 C.F.R. 63 subpart ZZZZ and of subpart A, including initial notification requirements:
 - a. Existing spark ignition 2 stroke lean burn (2SLB) stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions.

[45CSR34, 40 C.F.R. §63.6590(b)(3)(i)](E01, E02, E03, E04, E05, E06, E07)

- 5.1.2. If you own or operate any of the following stationary RICE with a site rating of more than 500 brake HP located at a major source of HAP emissions, you do not need to comply with the emission limitations in Tables 1a, 2a, 2c, and 2d to 40 C.F.R. 63 subpart ZZZZ or operating limitations in Tables 1b and 2b to 40 C.F.R. 63 subpart ZZZZ: an existing 2SLB stationary RICE; an existing 4SLB stationary RICE; a stationary RICE that combusts landfill gas or digester gas equivalent to 10 percent or more of the gross heat input on an annual basis; an emergency stationary RICE; or a limited use stationary RICE.
 [45CSR34, 40 C.F.R. §63.6600(c)](E01, E02, E03, E04, E05, E06, E07, G3, G4)
- 5.1.3. If you own or operate an emergency stationary RICE, you must operate the emergency stationary RICE according to the requirements in 40 C.F.R. §§63.6640(f)(1) through (3). In order for the engine to be considered an emergency stationary RICE under this subpart, any operation other than emergency operation, maintenance and testing, emergency demand response, and operation in non-emergency situations for 50 hours per year, as described in 40 C.F.R. §§63.6640(f)(1) through (3), is prohibited. If you do not operate the engine according to the requirements in paragraphs 40 C.F.R. §§63.6640(f)(1) through (3), the engine will not be considered an emergency engine under this subpart and must meet all requirements for non-emergency engines.
 - a. There is no time limit on the use of emergency stationary RICE in emergency situations.
 - b. You may operate your emergency stationary RICE for any combination of the purposes specified in 40 C.F.R. §63.6640(f)(2)(i) for a maximum of 100 hours per calendar year. Any operation for nonemergency situations as allowed by paragraphs 40 C.F.R. §63.6640(f)(3) counts as part of the 100 hours per calendar year allowed by this 40 C.F.R. §63.6640(f)(2).
 - i. Emergency stationary RICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor, the regional transmission organization or equivalent balancing authority and transmission operator, or the insurance company associated with the engine. The owner or operator may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if the owner or operator maintains records indicating that federal, state, or local standards require maintenance and testing of emergency RICE beyond 100 hours per calendar year.
 - c. Emergency stationary RICE located at major sources of HAP may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing and emergency demand response provided in 40 C.F.R. §63.6640(f)(2). The 50 hours per year for non-emergency situations

cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to supply power to an electric grid or otherwise supply power as part of a financial arrangement with another entity.

[45CSR34; 40 C.F.R. §§63.6640(f)(1) through (3)](G3 and G4)

- 5.1.4. The Emergency Generators (EGs), Identified as 005G3 and 005G4, shall meet the following requirements:
 - a. The authorized EGs shall each be the make, model, and size as specified under Table 1.1, shall only be fired by pipeline-quality natural gas, and each shall not operate in excess of 500 hours per year (during periods of non-emergencies);
 - b. The maximum emissions from the Waukesha F3521GL Emergency Generator, identified as 005G3, shall not exceed the limits given in the following table:

Pollutant	PPH	TPY
СО	4.31	1.08
NO _X	2.44	0.61
VOC	1.63	0.41
Formaldehyde	0.34	0.09

c. The maximum emissions from the Waukesha VGF-P48GL Emergency Generator, identified as 005G4, shall not exceed the limits given in the following table:

Pollutant	PPH	TPY
СО	10.36	2.59
NO _X	5.18	1.30
VOC	2.59	0.65
Formaldehyde	0.49	0.12

d. 40 C.F.R 60, Subpart JJJJ

The Waukesha VGF-P48GL identified as 005G4 shall meet all applicable requirements under 40 C.F.R. 60, Subpart JJJJ including the following:

(1) Owners and operators of stationary SI ICE with a maximum engine power greater than or equal to 75 KW (100 HP) (except gasoline and rich burn engines that use LPG) must comply with the emission standards in 40 C.F.R. 60, Subpart JJJJ Table 1 for their stationary ICE

Engine	Maximum	Manufaatuma		F	Emission S	tandard	s ^(a)	
type and	Engine	Date		g/HP-ł	ır	ppm	vd at 1	5% O ₂
fuel	Power		NO _x	CO	VOC ^(d)	NO _x	CO	VOC ^(d)
Emergency	HP≥130	1/1/2009	2.0	4.0	1.0	160	540	86

 $^{(a)}$ Owners and operators of stationary non-certified SI engines may choose to comply with the emission standards in units of either g/HP-hr or ppmvd at 15% O₂.

^(b) For Purposes of this subpart, when calculating emissions of volatile organic compounds, emissions of formaldehyde should not be included.

[45CSR16, 40 C.F.R. §60.4233(e), 40 C.F.R. 60 subpart JJJJ Table 1]

- (2) The emergency generator shall meet the definition of "Emergency Stationary Internal Combustion Engine" as given under 40 C.F.R. §60.4248.
 [45CSR16, 40 C.F.R. §60.4248]
 [45CSR13, R13-1856, Condition 4.1.3.]
- 5.1.5. Owners and operators of stationary SI ICE must operate and maintain stationary SI ICE that achieve the emission standards as required in §60.4233 over the entire life of the engine.
 [45CSR16, 40 C.F.R. §60.4234](G4)
- 5.1.6. Starting on July 1, 2010, if the emergency stationary SI internal combustion engine that is greater than or equal to 500 HP that was built on or after July 1, 2010, does not meet the standards applicable to non-emergency engines, the owner or operator must install a non-resettable hour meter.
 [45CSR16, 40 C.F.R. §60.4237(a)](G4)
- 5.1.7. If you are an owner or operator of a stationary SI internal combustion engine and must comply with the emission standards specified in §60.4233(d) or (e), you must demonstrate compliance according to one of the methods specified in 40 C.F.R. §60.4243(b)(1) and (2).
 - a. Purchasing a non-certified engine and demonstrating compliance with the emission standards specified in §60.4233(d) or (e) and according to the requirements specified in §60.4244, as applicable, and according to 40 C.F.R. §60.4243(b)(2)(ii).
 - i. If you are an owner or operator of a stationary SI internal combustion engine greater than 500 HP, you must keep a maintenance plan and records of conducted maintenance and must, to the extent practicable, maintain and operate the engine in a manner consistent with good air pollution control practice for minimizing emissions. In addition, you must conduct an initial performance test and conduct subsequent performance testing every 8,760 hours or 3 years, whichever comes first, thereafter to demonstrate compliance.

[45CSR16, 40 C.F.R. §§60.4243(b), (b)(2), & (b)(2)(ii)](G4)

- 5.1.8. If you own or operate an emergency stationary ICE, you must operate the emergency stationary ICE according to the requirements in 40 C.F.R. §§60.4243(d)(1) through (3). In order for the engine to be considered an emergency stationary ICE under this subpart, any operation other than emergency operation, maintenance and testing, emergency demand response, and operation in non-emergency situations for 50 hours per year, as described in 40 C.F.R. §§60.4243(d)(1) through (3), is prohibited. If you do not operate the engine according to the requirements in 40 C.F.R. §§60.4243(d)(1) through (3), the engine will not be considered an emergency engine under this subpart and must meet all requirements for non-emergency engines.
 - a. There is no time limit on the use of emergency stationary ICE in emergency situations.
 - b. You may operate your emergency stationary ICE for any combination of the purposes specified in in 40 C.F.R. §60.4243(d)(2)(i) for a maximum of 100 hours per calendar year. Any operation for nonemergency situations as allowed by in 40 C.F.R. §60.4243(d)(3) counts as part of the 100 hours per calendar year allowed by this in 40 C.F.R. §60.4243(d)(2).
 - i. Emergency stationary ICE may be operated for maintenance checks and readiness testing, provided that the tests are recommended by federal, state or local government, the manufacturer, the vendor,

the regional transmission organization or equivalent balancing authority and transmission operator, or the insurance company associated with the engine. The owner or operator may petition the Administrator for approval of additional hours to be used for maintenance checks and readiness testing, but a petition is not required if the owner or operator maintains records indicating that federal, state, or local standards require maintenance and testing of emergency ICE beyond 100 hours per calendar year.

- c. Emergency stationary ICE may be operated for up to 50 hours per calendar year in non-emergency situations. The 50 hours of operation in non-emergency situations are counted as part of the 100 hours per calendar year for maintenance and testing and emergency demand response provided in 40 C.F.R. §60.4243(d)(2). Except as provided in 40 C.F.R. §60.4243(d)(3)(i), the 50 hours per year for non-emergency situations cannot be used for peak shaving or non-emergency demand response, or to generate income for a facility to an electric grid or otherwise supply power as part of a financial arrangement with another entity.
 - i. The engine is dispatched by the local balancing authority or local transmission and distribution system operator;
 - ii. The dispatch is intended to mitigate local transmission and/or distribution limitations so as to avert potential voltage collapse or line overloads that could lead to the interruption of power supply in a local area or region.
 - iii. The dispatch follows reliability, emergency operation or similar protocols that follow specific NERC, regional, state, public utility commission or local standards or guidelines.
 - iv. The power is provided only to the facility itself or to support the local transmission and distribution system.
 - v. The owner or operator identifies and records the entity that dispatches the engine and the specific NERC, regional, state, public utility commission or local standards or guidelines that are being followed for dispatching the engine. The local balancing authority or local transmission and distribution system operator may keep these records on behalf of the engine owner or operator.

[45CSR16, 40 C.F.R. §60.4243(d)](G4)

5.2. Monitoring Requirements

5.2.1. For the purposes of demonstrating compliance with the maximum hours of operation limits set forth in 5.1.4.a, the permittee shall maintain monthly and rolling twelve month records of the hours of operation of the emergency generators.
 [45CSR13, R13-1856, Condition 4.2.2.]

5.3. Testing Requirements

5.3.1. For the purposes of demonstrating compliance with the emissions standards of 5.1.4.c and 40 C.F.R. §60.4233(e), the permittee shall conduct an initial performance test within one year after initial startup. After the initial test, subsequent testing shall be conducted every 8,760 hours of operation or 3 years, whichever comes first. If the engine is not operational, the permittee must conduct the performance test immediately upon startup of the engine. These tests must be conducted within 10 percent of the 100 percent peak (or highest achievable) load and according to the requirements of §60.8, under the specific conditions that are specified by Table 2 of Subpart JJJJ of Part 60 – Requirements for Performance test, and in accordance with Condition 3.3.1. of this permit. Records of such testing shall be maintained in accordance with Condition 3.4.1 of this permit.

[45CSR13, R13-1856, Condition 4.3.2.b](G4)

- 5.3.2. Owners and operators of stationary SI ICE who conduct performance tests must follow the procedures in 40 C.F.R. §§60.4244(a) through (f).
 - a. Each performance test must be conducted within 10 percent of 100 percent peak (or the highest achievable) load and according to the requirements in §60.8 and under the specific conditions that are specified by Table 2 to this subpart.
 - b. You may not conduct performance tests during periods of startup, shutdown, or malfunction, as specified in §60.8(c). If your stationary SI internal combustion engine is non-operational, you do not need to startup the engine solely to conduct a performance test; however, you must conduct the performance test immediately upon startup of the engine.
 - c. You must conduct three separate test runs for each performance test required in this section, as specified in §60.8(f). Each test run must be conducted within 10 percent of 100 percent peak (or the highest achievable) load and last at least 1 hour.
 - d. To determine compliance with the NO_X mass per unit output emission limitation, convert the concentration of NO_X in the engine exhaust using Equation 1 of this section:

$$ER = \frac{C_d \times 1.912 \times 10^{-3} \times Q \times T}{HP - hr}$$
(Eq. 1)

Where:

 $ER = Emission rate of NO_X in g/HP-hr.$

 C_d = Measured NO_X concentration in parts per million by volume (ppmv).

 1.912×10^{-3} = Conversion constant for ppm NO_X to grams per standard cubic meter at 20 degrees Celsius.

Q = Stack gas volumetric flow rate, in standard cubic meter per hour, dry basis.

T = Time of test run, in hours.

HP-hr = Brake work of the engine, horsepower-hour (HP-hr).

e. To determine compliance with the CO mass per unit output emission limitation, convert the concentration of CO in the engine exhaust using Equation 2 of this section:

$$ER = \frac{C_d \times 1.164 \times 10^{-3} \times Q \times T}{HP - hr}$$
(Eq. 2)

Where:

ER = Emission rate of CO in g/HP-hr.

 C_d = Measured CO concentration in ppmv.

 1.164×10^{-3} = Conversion constant for ppm CO to grams per standard cubic meter at 20 degrees Celsius. Q = Stack gas volumetric flow rate, in standard cubic meters per hour, dry basis.

T = Time of test run, in hours.

HP-hr = Brake work of the engine, in HP-hr.

f. For purposes of this subpart, when calculating emissions of VOC, emissions of formaldehyde should not be included. To determine compliance with the VOC mass per unit output emission limitation, convert the concentration of VOC in the engine exhaust using Equation 3 of this section:

$$ER = \frac{C_d \times 1.833 \times 10^{-3} \times Q \times T}{HP - hr}$$
(Eq. 3)

Where:

ER = Emission rate of VOC in g/HP-hr.

 $C_d = VOC$ concentration measured as propane in ppmv.

- 1.833×10^{-3} = Conversion constant for ppm VOC measured as propane, to grams per standard cubic meter at 20 degrees Celsius.
- Q = Stack gas volumetric flow rate, in standard cubic meters per hour, dry basis.

T = Time of test run, in hours.

HP-hr = Brake work of the engine, in HP-hr.

g. If the owner/operator chooses to measure VOC emissions using either Method 18 of 40 CFR part 60, appendix A, or Method 320 of 40 CFR part 63, appendix A, then it has the option of correcting the measured VOC emissions to account for the potential differences in measured values between these methods and Method 25A. The results from Method 18 and Method 320 can be corrected for response factor differences using Equations 4 and 5 of this section. The corrected VOC concentration can then be placed on a propane basis using Equation 6 of this section.

$$RF_i = \frac{C_{Mi}}{C_{Ai}}$$
(Eq. 4)

Where:

 RF_i = Response factor of compound i when measured with EPA Method 25A.

 C_{Mi} = Measured concentration of compound i in ppmv as carbon.

 C_{Ai} = True concentration of compound i in ppmv as carbon.

$$C_{icorr} = RF_i \times C_{imeas}$$
 (Eq. 5)

Where:

 C_{icorr} = Concentration of compound i corrected to the value that would have been measured by EPA Method 25A, ppmv as carbon.

C_{imeas} = Concentration of compound i measured by EPA Method 320, ppmv as carbon.

$$C_{Peq} = 0.6098 \times C_{icorr} \tag{Eq. 6}$$

Where:

CPeq = Concentration of compound i in mg of propane equivalent per DSCM.

[45CSR16, 40 C.F.R. §60.4244](G4)

5.4. Recordkeeping Requirements

- 5.4.1. Owners and operators of all stationary SI ICE must keep records of the following information:
 - a. All notifications submitted to comply with 40 C.F.R. 60 subpart JJJJ and all documentation supporting any notification.
 - b. Maintenance conducted on the engine.
 - c. If the stationary SI internal combustion engine is a certified engine, documentation from the manufacturer that the engine is certified to meet the emission standards and information as required in 40 CFR parts 90, 1048, 1054, and 1060, as applicable.
 - d. If the stationary SI internal combustion engine is not a certified engine or is a certified engine operating in a non-certified manner and subject to 60.4243(a)(2), documentation that the engine meets the emission standards.

[45CSR16, 40 C.F.R. §60.4245(a)](G4)

5.4.2. For all stationary SI emergency ICE greater than or equal to 500 HP manufactured on or after July 1, 2010, that do not meet the standards applicable to non-emergency engines, the owner or operator of must keep records of the hours of operation of the engine that is recorded through the non-resettable hour meter. The owner or operator must document how many hours are spent for emergency operation, including what classified the operation as emergency and how many hours are spent for non-emergency operation. [45CSR16, 40 C.F.R. §60.4245(b)](G4)

5.5. Reporting Requirements

- 5.5.1. If you are required to submit an Initial Notification but are otherwise not affected by the requirements of this subpart, in accordance with §63.6590(b), your notification should include the information in §63.9(b)(2)(i) through (v), and a statement that your stationary RICE has no additional requirements and explain the basis of the exclusion (for example, that it operates exclusively as an emergency stationary RICE if it has a site rating of more than 500 brake HP located at a major source of HAP emissions).
 [45CSR34, 40 C.F.R. §63.6645(f)](G4)
- 5.5.2. If you own or operate an emergency stationary RICE with a site rating of more than 100 brake HP that operates or is contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in § 63.6640(f)(2)(ii) and (iii) or that operates for the purpose specified in § 63.6640(f)(4)(ii), you must submit an annual report according to the requirements in paragraphs (1) through (3) of this section.
 - 1. The report must contain the following information:
 - a. Company name and address where the engine is located.

- b. Date of report and beginning and ending dates of the reporting period.
- c. Engine site rating and model year.
- d. Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.
- e. Hours operated for the purposes specified in § 63.6640(f)(2)(ii) and (iii), including the date, start time, and end time for engine operation for the purposes specified in § 63.6640(f)(2)(ii) and (iii).
- f. Number of hours the engine is contractually obligated to be available for the purposes specified in § 63.6640(f)(2)(ii) and (iii).
- g. Hours spent for operation for the purpose specified in § 63.6640(f)(4)(ii), including the date, start time, and end time for engine operation for the purposes specified in § 63.6640(f)(4)(ii). The report must also identify the entity that dispatched the engine and the situation that necessitated the dispatch of the engine.
- h. If there were no deviations from the fuel requirements in § 63.6604 that apply to the engine (if any), a statement that there were no deviations from the fuel requirements during the reporting period.
- i. If there were deviations from the fuel requirements in § 63.6604 that apply to the engine (if any), information on the number, duration, and cause of deviations, and the corrective action taken.
- 2. The first annual report must cover the calendar year 2015 and must be submitted no later than March 31, 2016. Subsequent annual reports for each calendar year must be submitted no later than March 31 of the following calendar year.
- 3. The annual report must be submitted electronically using the subpart specific reporting form in the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through EPA's Central Data Exchange (CDX) (www.epa.gov/cdx). However, if the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, the written report must be submitted to the Administrator at the appropriate address listed in § 63.13.

[45CSR34; 40 C.F.R. §63.6650 (h)] (G3 and G4)

- 5.5.3. Owners and operators of stationary SI ICE that are subject to performance testing must submit a copy of each performance test as conducted in §60.4244 within 60 days after the test has been completed. Performance test reports using EPA Method 18, EPA Method 320, or ASTM D6348-03 (incorporated by reference see 40 CFR 60.17) to measure VOC require reporting of all QA/QC data. For Method 18, report results from sections 8.4 and 11.1.1.4; for Method 320, report results from sections 8.6.2, 9.0, and 13.0; and for ASTM D6348-03 report results of all QA/QC procedures in Annexes 1-7. [45CSR16; 40 C.F.R. §60.4245(d)] (G4)
- 5.5.4. If you own or operate an emergency stationary SI ICE with a maximum engine power more than 100 HP that operates or is contractually obligated to be available for more than 15 hours per calendar year for the purposes specified in § 60.4243(d)(2)(ii) and (iii) or that operates for the purposes specified in § 60.4243(d)(3)(i), you must submit an annual report according to the requirements in conditions (1) through (3) of this section.
 - 1. The report must contain the following information:
 - a. Company name and address where the engine is located.

- b. Date of the report and beginning and ending dates of the reporting period.
- c. Engine site rating and model year.
- d. Latitude and longitude of the engine in decimal degrees reported to the fifth decimal place.
- e. Hours operated for the purposes specified in § 60.4243(d)(2)(ii) and (iii), including the date, start time, and end time for engine operation for the purposes specified in § 60.4243(d)(2)(ii) and (iii).
- f. Number of hours the engine is contractually obligated to be available for the purposes specified in § 60.4243(d)(2)(ii) and (iii).
- g. Hours spent for operation for the purposes specified in § 60.4243(d)(3)(i), including the date, start time, and end time for engine operation for the purposes specified in § 60.4243(d)(3)(i). The report must also identify the entity that dispatched the engine and the situation that necessitated the dispatch of the engine.
- 2. The first annual report must cover the calendar year 2015 and must be submitted no later than March 31, 2016. Subsequent annual reports for each calendar year must be submitted no later than March 31 of the following calendar year.
- 3. The annual report must be submitted electronically using the subpart specific reporting form in the Compliance and Emissions Data Reporting Interface (CEDRI) that is accessed through EPA's Central Data Exchange (CDX) (www.epa.gov/cdx). However, if the reporting form specific to this subpart is not available in CEDRI at the time that the report is due, the written report must be submitted to the Administrator at the appropriate address listed in § 60.4.

[45CSR16; 40 C.F.R. §60.4245(e)] (G4)

5.6. Compliance Plan

5.6.1. None.

6.0 Source Specific Requirements [emission point ID(s): E10]

6.1. Limitations and Standards

- 6.1.1. The Solar Titan 250 combustion turbine (CT), identified as 00510, shall meet the following requirements:
 - a. The authorized CT shall be the make, model, and size as specified under Table 1.1 and shall only be fired by pipeline-quality natural gas;
 - b. With the exception of operation during "low-temperature mode" and low-load mode" as defined under 6.2.1(a), at all times the CT is in operation, the unit shall utilize SoLoNO_x dry low-NO_x combustor technology;
 - c. The CT shall be fired using good combustion practices;
 - d. The maximum emissions from the CT shall not exceed the limits (during specific operational scenarios) as given in the following table:

Dollutont	PI	TDV	
Ponutant	Normal ⁽¹⁾	Low-Load	
СО	12.06	7.25	54.65
NO _x	7.93	23.84	35.67
PM _{2.5} /PM ₁₀ /PM	1.47	n/a	6.44
SO_2	12.71	n/a	0.70
VOC	1.38	0.66	6.03
Formaldehyde	0.16	n/a	0.69

⁽¹⁾ Emission limit valid for temperatures $\geq 32^{\circ}F$

- e. The CT shall meet all applicable requirements under 40 C.F.R. 60 Subpart KKKK including the following:
 - (i) You must meet the emission limits for NO_x specified in Table 1 to this subpart.

Table 1 to Subpart KKKK of Part 60—Nitrogen Oxide Emission Limits for New Stationary Combustion Turbines

Combustion turbine type	Combustion turbine heat input at peak load (HHV)	NO _x emission standard
New turbine firing natural gas	>50 MMBtu/h and ≤850 MMBtu/h	25 ppm at 15 percent O ₂ or 150 ng/J of useful output (1.2 lb/MWh).

[45CSR16, 40 C.F.R. §60.4320(a), 40 C.F.R. 60, Subpart KKKK Table 1]

- (ii) If your turbine is located in a continental area, you must comply with either paragraph 40 C.F.R. §§60.4330(a)(1), (a)(2), or (a)(3). [45CSR16, 40 C.F.R §60.4330(a)]
 - (1) You must not cause to be discharged into the atmosphere from the subject stationary combustion turbine any gases which contain SO₂ in excess of 110 nanograms per Joule (ng/J)

(0.90 pounds per megawatt-hour (lb/MWh)) gross output; [45CSR16, 40 C.F.R §60.4330(a)(1)]

(2) You must not burn in the subject stationary combustion turbine any fuel which contains total potential sulfur emissions in excess of 26 ng SO₂/J (0.060 lb SO₂/MMBtu) heat input. If your turbine simultaneously fires multiple fuels, each fuel must meet this requirement. [45CSR16, 40 C.F.R §60.4330(a)(2)]

[45CSR13, R13-1856, Condition 4.1.2]

- 6.1.2. Operation and Maintenance or Air Pollution Control Equipment. The permittee shall, to the extent practicable, install, maintain, and operate all air pollution control equipment listed in Section 1.1 and associated monitoring equipment in a manner consistent with safety and good air pollution control practices for minimizing emissions, or comply with any more stringent limits set forth in this permit or as set forth by any State rule, Federal regulation, or alternative control plan approved by the Secretary. [45CSR13, R13-1856, Condition 4.1.6]
- 6.1.3. The permittee must operate and maintain the stationary combustion turbine, air pollution control equipment, and monitoring equipment in a manner consistent with good air pollution control practices for minimizing emissions at all times including during startup, shutdown, and malfunction.
 [45CSR16, 40 C.F.R §60.4333(a); 45CSR13, R13-1856, Condition 4.1.2.f]
- 6.1.4. If you are not using water or steam injection to control NO_X emissions, you must perform annual performance tests in accordance with 40 C.F.R. §60.4400 to demonstrate continuous compliance. If the NO_X emission result from the performance test is less than or equal to 75 percent of the NO_X emission limit for the turbine, you may reduce the frequency of subsequent performance tests to once every 2 years (no more than 26 calendar months following the previous performance test). If the results of any subsequent performance test

exceed 75 percent of the NO_X emission limit for the turbine, you must resume annual performance tests. [45CSR16, 40 C.F.R §60.4340(a)]

6.2. Monitoring Requirements

- 6.2.1. The Solar Titan 250 CT shall meet the following Monitoring, Compliance Demonstration, Recording and Reporting Requirements:
 - a. The permittee shall monitor and record the monthly amount of hours the CT operates in the following modes:
 - (i) Normal Mode = Load \ge 40%, Temperature > -20°F: SoLoNO_x operating;
 - (ii) Low-Temperature Mode = Temperature $\leq -20^{\circ}$ F: non-SoLoNO_x mode; and
 - (iii) Low-Load Mode = Load $\leq 40\%$ (includes startup/shutdown events): non-SoLoNO_x mode.
 - b. To determine compliance with the CT annual emission limits given in 6.1.1.d, the permittee shall calculate the monthly and twelve month rolling average of actual emissions (in tons) that the CT emitted. The calculation of actual monthly and annual emissions shall be in accordance with the following:
 - (i) The permittee shall, by the 15th of each calendar month, calculate the actual monthly and rolling twelve month total of emissions of the CT using the data recorded under 6.2.1.a and the best available emission factors in accordance with the following requirements:

- (1) Emission factors may be used that were measured during the most recent performance test approved by the Secretary (and that were used to determine compliance with the hourly limits given in 6.1.1.d);
- (2) When emission factors as described under 6.2.1.b.(i)(1) are not available, the permittee shall use the emission factors used to calculate the potential-to-emit of the CT as given in Permit Application R13-1856A.

c. 40 C.F.R. 60, Subpart KKKK

You may elect not to monitor the total sulfur content of the fuel combusted in the turbine, if the fuel is demonstrated not to exceed potential sulfur emissions of 26 ng SO₂/J (0.060 lb/MMBtu) heat input for units located in continental areas and 180 ng SO₂/J (0.42 lb/MMBtu) heat input for units located in noncontinental areas or a continental area that the Administrator determines does not have access to natural gas and that the removal of sulfur compounds would cause more environmental harm than benefit. You must use one of the following sources of information to make the required demonstration:

- (i) The fuel quality characteristics in a current, valid purchase contract, tariff sheet or transportation contract for the fuel, specifying that the maximum total sulfur content for oil use in continental areas is 0.05 weight percent (500 ppmw) or less and 0.04 weight percent (4,000 ppmw) or less for noncontinental areas, the total sulfur content for natural gas use in continental areas is 20 grains of sulfur or less per 100 standard cubic feet and 140 grains of sulfur or less per 100 standard cubic feet for noncontinental areas, has potential sulfur emissions of less than 26 ng SO₂/J (0.060 lb SO₂/MMBtu) heat input for continental areas and has potential sulfur emissions of less than 180 ng SO₂/J (0.42 lb SO₂/MMBtu) heat input for noncontinental areas; or
- (ii) Representative fuel sampling data which show that the sulfur content of the fuel does not exceed 26 ng SO₂/J (0.060 lb SO₂/MMBtu) heat input for continental areas or 180 ng SO₂/J (0.42 lb SO₂/MMBtu) heat input for noncontinental areas. At a minimum, the amount of fuel sampling data specified in section 2.3.1.4 or 2.3.2.4 of appendix D to part 75 of this chapter is required.
 [45CSR16, 40 CFR §60.4365]

[45CSR13, R13-1856, Condition 4.2.1]

6.2.2. If you elect not to demonstrate sulfur content using options in 40 C.F.R. §60.4365, and the fuel is supplied without intermediate bulk storage, the sulfur content value of the gaseous fuel must be determined and recorded once per unit operating day.
 [45CSR16, 40 CFR§ 60.4370(b)]

6.3. Testing Requirements

- 6.3.1. The permittee shall meet the following testing requirement with respect to the Solar Titan 250 CT:
 - a. For the purposes of demonstrating compliance with the NO_x emission standard in condition 6.1.1.e and 40 C.F.R. §60.4320(a) the permittee shall conduct an initial performance test within 60 days after achieving maximum output of each turbine, but no later than 180 days after initial startup. After the initial test, subsequent performance testing shall be conducted annually (no more than 14 months following the previous test) unless the previous results demonstrate that the affected units achieved compliance of less than or equal to 75 percent of the NO_x emission limit, then the permittee may reduce

the frequency of subsequent tests to once every two years (no more than 26 calendar months following the previous test) as allowed under 40 C.F.R. 60.4320(a). If the results of any subsequent performance test exceed 75 percent of the NO_x emission limit, then the permittee must resume annual performance tests. Such testing shall be conducted in accordance with Condition 3.3.1. and 40 C.F.R. 60.4400. Records of such testing shall be maintained in accordance with Condition 3.4.2.

[45CSR13, R13-1856, Condition 4.3.2.a]

- 6.3.2. You must conduct an initial performance test, as required in §60.8. Subsequent NO_X performance tests shall be conducted on an annual basis (no more than 14 calendar months following the previous performance test).
 - a. There are two general methodologies that you may use to conduct the performance tests. For each test run:
 - i. Measure the NO_X concentration (in parts per million (ppm)), using EPA Method 7E or EPA Method 20 in appendix A of this part. For units complying with the output based standard, concurrently measure the stack gas flow rate, using EPA Methods 1 and 2 in appendix A of this part, and measure and record the electrical and thermal output from the unit. Then, use the following equation to calculate the NO_X emission rate:

$$E = \frac{(1.194 \times 10^{-7}) \times (NO_X)_C \times Q_{std}}{P}$$

Where:

 $E = NO_X$ emission rate, in lb/MWh

 1.194×10^{-7} = conversion constant, in lb/dscf-ppm

 $(NO_X)_c$ = average NO_X concentration for the run, in ppm

 $Q_{std} = stack$ gas volumetric flow rate, in dscf/hr

- P = gross electrical and mechanical energy output of the combustion turbine, in MW (for simplecycle operation), for combined-cycle operation, the sum of all electrical and mechanical output from the combustion and steam turbines, or, for combined heat and power operation, the sum of all electrical and mechanical output from the combustion and steam turbines plus all useful recovered thermal output not used for additional electric or mechanical generation, in MW, calculated according to 60.4350(f)(2); or
- ii. Measure the NO_X and diluent gas concentrations, using either EPA Methods 7E and 3A, or EPA Method 20 in appendix A of this part. Concurrently measure the heat input to the unit, using a fuel flowmeter (or flowmeters), and measure the electrical and thermal output of the unit. Use EPA Method 19 in appendix A of this part to calculate the NO_X emission rate in lb/MMBtu. Then, use Equations 1 and, if necessary, 2 and 3 in §60.4350(f) to calculate the NO_X emission rate in lb/MWh.
- b. Sampling traverse points for NO_X and (if applicable) diluent gas are to be selected following EPA Method 20 or EPA Method 1 (non-particulate procedures), and sampled for equal time intervals. The sampling must be performed with a traversing single-hole probe, or, if feasible, with a stationary multi-hole probe that samples each of the points sequentially. Alternatively, a multi-hole probe designed and documented to sample equal volumes from each hole may be used to sample simultaneously at the required points.
- c. Notwithstanding 40 C.F.R. §60.4400(a)(2), you may test at fewer points than are specified in EPA Method 1 or EPA Method 20 in appendix A of this part if the following conditions are met

- i. You may perform a stratification test for NOX and diluent pursuant to the procedures specified in section 6.5.6.1(a) through (e) of appendix A of part 75 of this chapter.
- ii. Once the stratification sampling is completed, you may use the following alternative sample point selection criteria for the performance test:
 - A. If each of the individual traverse point NO_X concentrations is within ± 10 percent of the mean concentration for all traverse points, or the individual traverse point diluent concentrations differs by no more than ± 5 ppm or ± 0.5 percent CO₂ (or O₂) from the mean for all traverse points, then you may use three points (located either 16.7, 50.0 and 83.3 percent of the way across the stack or duct, or, for circular stacks or ducts greater than 2.4 meters (7.8 feet) in diameter, at 0.4, 1.2, and 2.0 meters from the wall). The three points must be located along the measurement line that exhibited the highest average NO_X concentration during the stratification test; or
 - B. For turbines with a NO_X standard greater than 15 ppm @ 15% O₂, you may sample at a single point, located at least 1 meter from the stack wall or at the stack centroid if each of the individual traverse point NO_X concentrations is within ±5 percent of the mean concentration for all traverse points, or the individual traverse point diluent concentrations differs by no more than ±3ppm or ±0.3 percent CO₂ (or O₂) from the mean for all traverse points; or
 - C. For turbines with a NO_X standard less than or equal to 15 ppm @ 15% O₂, you may sample at a single point, located at least 1 meter from the stack wall or at the stack centroid if each of the individual traverse point NO_X concentrations is within ± 2.5 percent of the mean concentration for all traverse points, or the individual traverse point diluent concentrations differs by no more than ± 1 ppm or ± 0.15 percent CO₂ (or O₂) from the mean for all traverse points.

[45CSR16, 40 C.F.R. §60.4400(a)]

- 6.3.3. The performance test must be done at any load condition within plus or minus 25 percent of 100 percent of peak load. You may perform testing at the highest achievable load point, if at least 75 percent of peak load cannot be achieved in practice. You must conduct three separate test runs for each performance test. The minimum time per run is 20 minutes.
 - a. If the stationary combustion turbine combusts both oil and gas as primary or backup fuels, separate performance testing is required for each fuel.
 - b. For a combined cycle and CHP turbine systems with supplemental heat (duct burner), you must measure the total NO_X emissions after the duct burner rather than directly after the turbine. The duct burner must be in operation during the performance test.
 - c. If water or steam injection is used to control NO_X with no additional post-combustion NO_X control and you choose to monitor the steam or water to fuel ratio in accordance with §60.4335, then that monitoring system must be operated concurrently with each EPA Method 20 or EPA Method 7E run and must be used to determine the fuel consumption and the steam or water to fuel ratio necessary to comply with the applicable §60.4320 NO_X emission limit.

- d. Compliance with the applicable emission limit in §60.4320 must be demonstrated at each tested load level. Compliance is achieved if the three-run arithmetic average NO_X emission rate at each tested level meets the applicable emission limit in §60.4320.
- e. If you elect to install a CEMS, the performance evaluation of the CEMS may either be conducted separately or (as described in §60.4405) as part of the initial performance test of the affected unit.
- f. The ambient temperature must be greater than 0 °F during the performance test.

[45CSR16, 40 C.F.R. §60.4400(b)]

6.4. Recordkeeping Requirements

- 6.4.1. Record of Maintenance of Air Pollution Control Equipment. For all pollution control equipment listed in section 1.1, the permittee shall maintain accurate records of all required pollution control equipment inspection and/or preventative maintenance procedures.
 [45CSR13, R13-1856, Condition 4.4.2]
- 6.4.2. **Record of Malfunctions of Air Pollution Control Equipment.** For all air pollution control equipment listed in section 1.1, the permittee shall maintain records of the occurrence and duration of any malfunction or operational shutdown of the air pollution control equipment during which excess emissions occur. For each such case, the following information shall be recorded:
 - a. The equipment involved.
 - b. Steps taken to minimize emissions during the event.
 - c. The duration of the event.
 - d. The estimated increase in emissions during the event.

For each such case associated with an equipment malfunction, the additional information shall also be recorded:

- e. The cause of the malfunction.
- f. Steps taken to correct the malfunction.
- g. Any changes or modifications to equipment or procedures that would help prevent future reoccurrences of the malfunction.

[45CSR13, R13-1856, Condition 4.4.3]

6.5. **Reporting Requirements**

6.5.1. For each affected unit required to continuously monitor parameters or emissions, or to periodically determine the fuel sulfur content under this subpart, you must submit reports of excess emissions and monitor downtime, in accordance with §60.7(c). Excess emissions must be reported for all periods of unit operation, including start-up, shutdown, and malfunction.

[45CSR16, 40 C.F.R §60.4375(a)]

6.5.2. For each affected unit that performs annual performance tests in accordance with §60.4340(a), you must submit a written report of the results of each performance test before the close of business on the 60th day following the completion of the performance test.
 [45CSR16, 40 C.F.R §60.4375(b)]

6.6. Compliance Plan

6.6.1. None.

West Virginia Department of Environmental Protection Division of Air Quality





For Draft/Proposed Renewal Permitting Action Under 45CSR30 and Title V of the Clean Air Act

Permit Number: **R30-09900013-2022** Application Received: **May 26, 2022** Plant Identification Number: **099-00013** Permittee: **Columbia Gas Transmission, LLC** Facility Name: **Ceredo Compressor Station** Mailing Address: **1700 MacCorkle Avenue, SE, Charleston, WV 25314**

Revised: N/A

Physical Location: UTM Coordinates: Directions: Walkers Branch Road, Wayne County, West Virginia
366.1 km Easting • 4247.7 km Northing • Zone 17
Traveling I-64 West from Charleston, take the Kenova-Ceredo exit.
Turn left onto Route 52. Make a left onto Airport Road. Turn right onto
Walkers Branch Road at the Pilgrim Glass Plant, travel 2 miles, the
station is on the left.

Facility Description

The Ceredo Station is a natural gas transmission facility covered by Standard Industrial Code (SIC) 4922. The station has the potential to operate seven (7) days per week, twenty-four (24) hours per day. The station consists of six (6) 2800-hp and one (1) 2700-hp natural gas fired reciprocating compressor engines, one (1) 30,399-hp compressor turbine, and numerous storage tanks of various sizes. On-site support equipment includes one (1) 812 hp and one (1) 1,175 hp emergency generators, one (1) 6.276 MMBtu/hr boiler, and one (1) 0.375 MMBtu/hr and one (1) 0.60 MMBtu/hr line heaters.

Emissions Summary

Plantwide Emissions Summary [Tons per Year]				
Regulated Pollutants	Potential Emissions	2020 Actual Emissions		
Carbon Monoxide (CO)	310.41	40.86		
Nitrogen Oxides (NO _X)	3,582.71	403.14		
Particulate Matter (PM _{2.5})	41.03	5.06		
Particulate Matter (PM ₁₀)	41.03	5.06		
Total Particulate Matter (TSP)	41.03	5.06		
Sulfur Dioxide (SO ₂)	1.23	0.19		
Volatile Organic Compounds (VOC)	107.30	15.87		

PM_{10} is a component of TSP.

Hazardous Air Pollutants	Potential Emissions	2020 Actual Emissions
Benzene	1.39	NA
Toluene	0.81	NA
Ethylbenzene	0.11	NA
Xylene	0.19	NA
n-Hexane	0.38	NA
Formaldehyde	40.11	4.45
Acetaldehyde	5.58	NA
Other HAPs	9.43	NA
Total HAPs	58.00	NA

Some of the above HAPs may be counted as PM or VOCs.

Title V Program Applicability Basis

This facility has the potential to emit 310.41 tons per year of Carbon Monoxide (CO), 3,582.71 tons per year of Nitrogen Oxides (NOx), 107.30 tons per year of Volatile Organic Compounds (VOC), 40.11 tons per year of Formaldehyde, and 58.00 tons per year of total HAPs. Due to this facility's potential to emit over 100 tons per year of criteria pollutant, over 10 tons per year of a single HAP, and over 25 tons per year of aggregate HAPs, Columbia Gas Transmission, LLC is required to have an operating permit pursuant to Title V of the Federal Clean Air Act as amended and 45CSR30.

Legal and Factual Basis for Permit Conditions

The State and Federally-enforceable conditions of the Title V Operating Permits are based upon the requirements of the State of West Virginia Operating Permit Rule 45CSR30 for the purposes of Title V of the Federal Clean Air Act and the underlying applicable requirements in other state and federal rules.

This facility has been found to be subject to the following applicable rules:

Federal and State:	45CSR2	PM limits for Indirect Heat Exchangers
	45CSR6	Open burning prohibited.
	45CSR11	Standby plans for emergency episodes.
	45CSR13	Construction permits
	45CSR16	Standards of Performance for New
		Stationary Sources.
	WV Code § 22-5-4 (a) (14)	The Secretary can request any pertinent
		information such as annual emission
		inventory reporting.
	45CSR30	Operating permit requirement.
	45CSR34	Emission Standards for HAPs
	40 C.F.R. 60, Subpart JJJJ	Standards of Performance for Stationary
		Spark Ignition Internal Combustion Engines
	40 C.F.R. 60, Subpart KKKK	Standards of Performance for Stationary
		Combustion Turbines
	40 C.F.R. Part 61	Asbestos inspection and removal
	40 C.F.R. 63, Subpart ZZZZ	National Emissions Standards for Hazardous
		Air Pollutants for Stationary Reciprocating
		Internal Combustion Engines
	40 C.F.R. 63, Subpart DDDDD	National Emission Standards for Hazardous
		Air Pollutants for Major Sources: Industrial,
		Commercial, and Institutional Boilers and
		Process Heaters
	40 C.F.R. Part 82, Subpart F	Ozone depleting substances
State Only:	45CSR4	No objectionable odors.
·	45CSR17	Prevent And Control Particulate Matter Air
		Pollution From Materials Handling,
		Preparation, Storage And Other Sources Of
		Fugitive Particulate Matter

Each State and Federally-enforceable condition of the Title V Operating Permit references the specific relevant requirements of 45CSR30 or the applicable requirement upon which it is based. Any condition of the Title V permit that is enforceable by the State but is not Federally-enforceable is identified in the Title V permit as such.

The Secretary's authority to require standards under 40 C.F.R. Part 60 (NSPS), 40 C.F.R. Part 61 (NESHAPs), and 40 C.F.R. Part 63 (NESHAPs MACT) is provided in West Virginia Code §§ 22-5-1 *et seq.*, 45CSR16, 45CSR34 and 45CSR30.

Active Permits/Consent Orders

Permit or	Date of	Permit Determinations or Amendments That
Consent Order Number	Issuance	Affect the Permit (<i>if any</i>)
R13-1856C	December 18, 2017	

Conditions from this facility's Rule 13 permit(s) governing construction-related specifications and timing requirements will not be included in the Title V Operating Permit but will remain independently enforceable under the applicable Rule 13 permit(s). All other conditions from this facility's Rule 13 permit(s) governing the source's operation and compliance have been incorporated into this Title V permit in accordance with the "General Requirement Comparison Table," which may be downloaded from DAQ's website.

Determinations and Justifications

R30-09900013-2016 (SM01) was issued on August 28, 2017 to incorporate the changes approved under R13-1856B issued on July 13, 2017. On December 18, 2017, Class I administrative update R13-1856C was issued to reduce the maximum design heat input of HTR 3 from 1.0 to 0.6 MMBtu/hr and to add three (3) de minimis storage tanks. Since the permittee did not submit a modification to the Title V permit for the changes approved under R13-1856C, they will be incorporated into this Title V renewal.

The following changes and updates have been made to the Title V permit during this renewal:

Section 1.0

- The Emission Units Table was updated to reflect the changes in R13-1856C. The design capacity of HTR3 was changed from 1.0 to 0.60 MMBtu/hr, the 900 gallon oil-water storage tank was added, the 5,000 gallon waste water storage tank was added, and the 5,000 gallon condensate storage tank was added.
- Table 1.2 was updated since R13-1856C supersedes and replaces R13-1856B.

Section 3.0

- Permit condition 3.1.12 was updated to match the latest version of 40 C.F.R. §60.5397a.
- Permit condition 3.5.3 was updated to match the most recent boilerplate.
- Deleted the last paragraph in condition 3.1.9 since this language is not in R13-1856C.
- Moved condition 3.4.4 to the Limits and Standards section as condition 3.1.13 since it is not a recordkeeping requirement.

Section 4.0

• Permit condition 4.1.11 was updated to reflect the changes in R13-1856C. Specifically, the MDHI in condition 4.1.11.a was changed from 1.00 to 0.60 MMBtu/hr and the emission limits in Table 4.1.1.c were updated to reflect the new limits in R13-1856C.

Section 5.0

- Deleted vacated sections 40 C.F.R. §§63.6640(f)(2)(ii) and (iii) from condition 5.1.3 and deleted vacated sections 40 C.F.R. §§60.4243(d)(2)(ii) and (iii) from condition 5.1.8
- Added reporting requirements for G3 and G4 from 40 CFR §60.6650(h) as condition 5.5.2
- Added reporting requirements for G4 from 40 CFR §§60.4245(d) and (e) as conditions 5.5.3 and 5.5.4

Non-Applicability Determinations

The following requirements have been determined not to be applicable to the subject facility due to the following:

According to 45CSR§2-11.1 the boiler and heaters are exempt from the weight emission standards and MRR (monitoring, recordkeeping and reporting) because they are less than 10 mmBtu/hr.

45CSR10; *To Prevent and Control Air Pollution from The Emission of Sulfur Oxides*: 45CSR10 is not applicable to the facility boiler and heaters because they are less than 10 mmBtu/hr.

45CSR21; *To Prevent and Control Air Pollution from the Emission of Volatile Organic Compounds:* All storage tanks at Ceredo station are below 40,000 gallons in capacity, hence 45CSR§21-28 is not applicable. Ceredo station is not engaged in the extraction or fractionation of natural gas, hence, 45CSR§21-29 is not applicable.

45CSR27; *To Prevent and Control the Emissions of Toxic Air Pollutants:* Natural gas is included as a petroleum product and contains less than 5% benzene by weight. 45CSR§27-2.4 exempts equipment "used in the production and distribution of petroleum products providing that such equipment does not produce or contact materials containing more than 5% benzene by weight."

40 C.F.R. 60 Subpart Dc; *Standards of Performance for Steam Generating Units:* The boiler and heaters at this facility are less than 10 mmBtu/hr; hence, Subpart Dc is not applicable.

40 C.F.R. 60 Subparts K,Ka; *Standards of Performance for Storage Vessels for Petroleum Liquids:* All tanks at Ceredo station are below 40,000 gallons in capacity.

40 C.F.R. 60 Subpart Kb; *Standards of Performance for Volatile Organic Liquid Storage Vessels:* All tanks at Ceredo station are below 75m³ in capacity.

40 C.F.R. 60 Subpart KKK; *Standards of Performance for Equipment Leaks of VOC From Onshore Natural Gas Processing Plant:* Ceredo station is not engaged in the extraction or fractionation of natural gas liquids from field gas, the fractionation of mixed natural gas liquids to natural gas products, or both.

40 C.F.R. 60 Subpart IIII; *Standards of Performance for Stationary Compression Ignition Internal Combustion Engines*: There are no compression ignition engines at this facility.

40 C.F.R 60 Subpart OOOO; Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution: Storage vessel requirements do not apply since all tanks commenced construction prior to August 23, 2011.

40 C.F.R. 63 Subpart HHH; *National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities*: The facility does not have a glycol dehydration unit and is therefore not subject to the requirements of this subpart.

40 C.F.R. 63 Subpart YYYY; Turbine *MACT:* The Solar Titan 250 (E10) is subject to 40 C.F.R. 63 Subpart YYYY. Per 40 C.F.R. §63.6095(d), there is a stay of standards for lean premix stationary combustion turbines until EPA takes final action to require compliance with this subpart. The only requirement for the unit is the initial notification requirement of 40 C.F.R. §63.6145, which was satisfied by the preconstruction permit application.

40 C.F.R. 64 - None of the emission units have any add-on controls; therefore, in accordance with 40 C.F.R § 64.2(a), CAM is not applicable to this facility.

Request for Variances or Alternatives

None.

Insignificant Activities

Insignificant emission unit(s) and activities are identified in the Title V application.

Comment Period

Beginning Date: Ending Date:

Point of Contact

All written comments should be addressed to the following individual and office:

Nikki Moats West Virginia Department of Environmental Protection Division of Air Quality 601 57th Street SE Charleston, WV 25304 Phone: 304/926-0499 ext. 41282 Nikki.B.Moats@wv.gov

Procedure for Requesting Public Hearing

During the public comment period, any interested person may submit written comments on the draft permit and may request a public hearing, if no public hearing has already been scheduled. A request for public hearing shall be in writing and shall state the nature of the issues proposed to be raised in the hearing. The Secretary shall grant such a request for a hearing if he/she concludes that a public hearing is appropriate. Any public hearing shall be held in the general area in which the facility is located.

Response to Comments (Statement of Basis)

Division of Air Quality Permit Application Submittal

Please find attached a permit application for : Columbia Gas Transmission, LLC, Ceredo Compressor Station [Company Name: Facility Location] DAQ Facility ID (for existing facilities only): 099-00013 • Current 45CSR13 and 45CSR30 (Title V) permits associated with this process (for existing facilities only): R30-09900013-2016 (SM01) and R13-1856C Type of NSR Application (check all that apply): Type of 45CSR30 (TITLE V) Application: □ Construction □ Title V Initial ☐ Modification ☑ Title V Renewal **Class I Administrative Update** □ Administrative Amendment** Class II Administrative Update □ Minor Modification** **☐** Relocation □ Significant Modification** **Temporary** □ Off Permit Change ** If the box above is checked, include the Title V **Permit Determination** revision information as ATTACHMENT S to the combined NSR/Title V application. **Payment Type:** • □ Credit Card (Instructions to pay by credit card will be sent in the Application Status email.) □ Check (Make checks payable to: WVDEP – Division of Air Quality) **Please wait until DAQ** Mail checks to: emails you the Facility WVDEP - DAQ - Permitting **D** Number and Permit **Attn: NSR Permitting Secretary** Application Number. 601 57th Street, SE **Please add these** Charleston. WV 25304 identifiers to your check or cover letter with your check. If the permit writer has any questions, please contact (all that apply): • **Responsible Official/Authorized Representative** • Name: [Email: [• • **Phone Number:** Company Contact Name: Trevor Galley • Email: trevor_galley@tcenergy.com • • Phone Number: 304-357-2076 □ Consultant • Name: Email: | ۲ Phone Number: •



Columbia Gas Transmission, LLC

Air Permit Application for Renewal Ceredo Natural Gas Compressor Station

Ceredo, West Virginia



ENVIRONMENTAL RESOURCES MANAGEMENT, Inc. Hurricane, West Virginia

May 2021

Columbia Gas Transmission, LLC 1700 MacCorkle Avenue SE Charleston, WV 25314



May 26, 2021

Director WV Department of Environmental Protection (WVDEP) Division of Air Quality (DAQ) 601 57th Street SE Charleston, WV 25304

Re: Columbia Gas Transmission, LLC (Columbia) Ceredo Compressor Station (Facility ID: 099-00013) Title V Operating Permit Renewal Application

Dear Director,

In accordance WV 45CSR30, please find the attached Title V permit renewal application for Columbia's Ceredo Compressor Station, which is located in Wayne County, West Virginia. Ceredo Compressor Station currently operates under Permit No. R30-09900013-2016 under 45CSR30. The current Title V Permit to Operate expires on December 27, 2021.

This package contains the general application forms along with the required attachments for a Title V renewal permit application. Ceredo Compressor Station's Potential to Emit (PTE) exceeds 100 tons per year for Nitrogen Oxides (NO_x) and Carbon Monoxide (CO) and Volatile Organic Compounds (VOCs). The Ceredo Compressor Station also qualifies as a major source of Hazardous Air Pollutants (HAPs), since the PTE exceeds major source thresholds for formaldehyde and aggregate HAPs. For these reasons, Ceredo in considered a Title V source for permitting purposes.

Should you have any questions regarding the application or if additional information is required, please contact me by email at <u>trevor_galley@tcenergy.com</u>.

Sincerely,

Trevor Galley Environmental Analyst TC Energy

OF WEST VIA	WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION
	DIVISION OF AIR QUALITY
	601 57 th Street SE
SEMPER LIGHT	Charleston, WV 25304
	Phone: (304) 926-0475
	www.dep.wv.gov/daq
INITIAL/RENE	WAL TITLE V PERMIT APPLICATION - GENERAL FORMS

Section 1: General Information

1. Name of Applicant (As registered with the WV Secretary of State's Office):	2. Facility Name or Location:	
Columbia Gas Transmission, LLC	Ceredo Compressor Station	
3. DAQ Plant ID No.:	4. Federal Employer ID No. (FEIN):	
099-00013	310802435	
5. Permit Application Type:		
 ☐ Initial Permit When did op ✓ Permit Renewal What is the op ☐ Update to Initial/Renewal Permit Application 	perations commence? expiration date of the existing permit?	
6. Type of Business Entity:	7. Is the Applicant the:	
□ Corporation □ Governmental Agency ☑ LLC □ Partnership □ Limited Partnership	Owner Operator Both	
8. Number of onsite employees: Less than ten (10) employees	please provide the name and address of the other party.	
9. Governmental Code:		
 Privately owned and operated; 0 County government owned and operated; 3 Federally owned and operated; 1 Municipality government owned and operated; 4 District government owned and operated; 5 		
10. Business Confidentiality Claims		
Does this application include confidential information (per 45CSR31)? Yes No		
If yes, identify each segment of information on each page that is submitted as confidential, and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's " <i>PRECAUTIONARY NOTICE-CLAIMS OF CONFIDENTIALITY</i> " guidance.		

11. Mailing Address						
Street or P.O. Box: 1700 MacCorkle Avenue, SE						
City: Charleston State: WV Zip: 25314						
Telephone Number: (304) 357 - 2047 Fax Number: (304) 357 - 2770						

12. Facility Location		
Street: 1664 Walkers Branch Road	City: Huntington	County: Wayne
UTM Easting: 366.115 km	UTM Northing: 4247.720 km	Zone: Z 17 or 1 8
Directions: Traveling I-64 West fro	om Charleston, take the Kenova-Ce	redo exit. Turn left onto Route 52.
Make a left onto Airport Road. Turn r	ight onto Walker's Branch Road at the F	Pilgrim Glass Plant, and travel 2 miles;
the station is on the left.		
Portable Source? Yes	No	
Is facility located within a nonattain	nment area? 🗌 Yes 🗹 No	If yes, for what air pollutants?
Is facility located within 50 miles of	another state? 🗹 Yes 🗌 No	If yes, name the affected state(s).
		Kentucky
		Ohio
Is facility located within 100 km of	a Class I Area ¹ ? 🗌 Yes 📝 No	If yes, name the area(s).
If no, do emissions impact a Class I	Areal? Ves V No	
in no, ao emissions impact a Class I		
1 Class Lareas include Dolly Sods and Ottor	Creek Wilderness Areas in West Virginia and Sl	henandoah National Park and James Piver
Face Wilderness Area in Virginia.		

13. Contact Information			
Responsible Official: Richard Smith		Title: Operations Manager	
Street or P.O. Box: 1700 MacCorkle Avenue, SE			
City: Charleston	State: WV	Zip: 25314	
Telephone Number: 304-984-4603	Fax Number: () -		
E-mail address: richard_smith@tcenerg	ly.com		
Environmental Contact: Trevor Galley Title: Environmental		Title: Environmental Analyst	
Street or P.O. Box: 1700 MacCorkle Avenue, SE			
City: Charleston	State: WV	Zip: 25314	
Telephone Number: (304) 357 - 2076 Fax Number: () -			
E-mail address: trevor_galley@tcenergy.com			
Application Preparer: Grant Morgan		Title: Principal Consultant	
Company: ERM (Environmental Resources Managment)			
Street or P.O. Box: 204 Chase Drive			
City: Hurricane	State: WV Zip: 25526		
Telephone Number: (304) 590 - 6160	Fax Number: () -		
E-mail address: Grant.Morgan@erm.co	om		

14. Facility Description

List all processes, products, NAICS and SIC codes for normal operation, in order of priority. Also list any process, products, NAICS and SIC codes associated with any alternative operating scenarios if different from those listed for normal operation.

Process	Products	NAICS	SIC
Natural Gas Transmission	Natural Gas	486210	4922

Provide a general description of operations.

The Ceredo Compressor Station is a natural gas transmission facility covered by Standard Industrial Classification (SIC) Code 4922. The station includes seven (7) gas-drive reciprocating compressors, four (4) electric-drive turbines, one (1) gas-drive turbine, two (2) emergency generators, one (1) boiler, two (2) process heaters, and various tanks.

15. Provide an Area Map showing plant location as ATTACHMENT A.

16. Provide a **Plot Plan(s)**, e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is located as **ATTACHMENT B**.

For instructions, refer to "Plot Plan - Guidelines."

 Provide a detailed Process Flow Diagram(s) showing each process or emissions unit as ATTACHMENT C. Process Flow Diagrams should show all emission units, control equipment, emission points, and their relationships.

18. Applicable Requirements Summary				
Instructions: Mark all applicable requirements.				
SIP	□ FIP			
Minor source NSR (45CSR13)	□ PSD (45CSR14)			
✓ NESHAP (45CSR34)	□ Nonattainment NSR (45CSR19)			
Section 111 NSPS	Section 112(d) MACT standards			
Section 112(g) Case-by-case MACT	□ 112(r) RMP			
Section 112(i) Early reduction of HAP	Consumer/commercial prod. reqts., section 183(e)			
Section 129 Standards/Reqts.	Stratospheric ozone (Title VI)			
Tank vessel reqt., section 183(f)	Emissions cap 45CSR§30-2.6.1			
□ NAAQS, increments or visibility (temp. sources)	☐ 45CSR27 State enforceable only rule			
✓ 45CSR4 State enforceable only rule	Acid Rain (Title IV, 45CSR33)			
Emissions Trading and Banking (45CSR28)	Compliance Assurance Monitoring (40CFR64)			
\Box CAIR NO _x Annual Trading Program (45CSR39)	CAIR NO _x Ozone Season Trading Program (45CSR40)			
\Box CAIR SO ₂ Trading Program (45CSR41)				

19. Non Applicability Determinations

List all requirements which the source has determined not applicable and for which a permit shield is requested. The listing shall also include the rule citation and the reason why the shield applies.

45CSR4 – To Prevent and Control the Discharge of Air Pollutants into the Open Air Which Causes or Contributes to an Objectionable Odor or Odors: According to 45CSR§4-7.1, this rule shall not apply to the following sources of objectionable odor until such time as feasible control methods are developed: Internal Combustion Engines

45CSR10 – To Prevent and Control Air Pollution from the Emission of Sulfur Oxides: 45CSR10 is not applicable to the facility's heater because its maximum design heat input (DHI) is less than 10 MMBtu/hr

45CSR21 – To Prevent and Control Air Pollution from the Emission of Volatile Organic Compounds: All storage tanks at the station, which are listed as insignificant sources, are below 40,000 gallons in capacity which exempts the facility from 45CSR§21-28.

The compressor station is not engaged in the extraction or fractionation of natural gas which exempts the facility from 45CSR§21-29 45CSR27 – ToPrevent and Control the Emissions of Toxic Air Pollutants: Natural gas is included as a petroleum product and contains less than 5% benzene by weight. 45CSR§27-2.4 exempts equipment "used in the production and distribution of petroleum products providing that such equipment does not produce or contact materials containing more than 5% benzene by weight."

Permit Shield

 \checkmark

19. No	on Applicability	Determinations	(Continued) - Attach	additional	pages	as necessary
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List all requirements which the source has determined not applicable and for which a permit shield is requested. The listing shall also include the rule citation and the reason why the shield applies.

 $40 \text{ CFR } 60 \text{ Subpart } \text{GG} - \text{Standards of Performance for Stationary Gas Turbines: The two turbines on site were installed in 1967 and 1971 which predates this NSPS's applicability trigger date of October 3, 1977 as defined in §60.330(b).$

40 CFR 60 Subparts K,Ka – Standards of Performance for Storage Vessels for Petroleum Liquids: All tanks at the facility are below 40,000 gallons in capacity as specified in 60.110a(a).

40 CFR 60 Subpart Kb – Standards of Performance for Volatile Organic Liquid Storage Vessels: All tanks at the facility are below 75m3 (19,813 gallons) in capacity as specified in 60.110b(a).

40 CFR 60 Subpart KKK – Standards of Performance for Equipment Leaks of VOC From Onshore Natural Gas Processing Plant: This compressor station is not engaged in the extraction or fractionation of natural gas liquids from field gas, the fractionation of mixed natural gas liquids to natural gas products, or both.

40 CFR 60 Subpart IIII – Standards of Performance for Stationary Compression Ignition Internal Combustion Engines: There are no compression ignition engines at this facility.

40 CFR 60 Subpart JJJJ – Standards of Performance for Stationary Spark Ignition Internal Combustion Engines: All engines at the facility were constructed, reconstructed, or modified prior to the June 12, 2006 applicability date listed in 60.4230(a)(4).

40 CFR 60 Subpart OOOO – Standards of Performance for Crude Oil and Natural Gas Production, Transmission and Distribution: The Storage Vessel requirements defined for transmission sources is not applicable to this site because all vessels were constructed, commenced construction, prior to August 23, 2011 as stated in accordance with [40CFR§60.5365(e)].

40 CFR 63 Subpart HHH – National Emission Standards for Hazardous Air Pollutants from Natural gas Transmission and Storage Facilities: This facility does not have a glycol dehydration unit and is therefore not subject to the requirements of this subpart.

40 CFR 64 - Compliance Assurance Monitoring (CAM): There are no add-on controls at this facility; therefore, in accordance with 40 CFR (64.2(b)(1), CAM is not applicable to this facility.

Permit Shield

20. Facility-Wide Applicable Requirements

List all facility-wide applicable requirements. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*).

T5-3.1.1-45 CSR 6-3.1 - Open burning prohibited T5-3.1.2-45 CSR 6-3.2 - Open burning exemption stipulations T5-3.1.3-40 CFR Part 61 and 45 CSR 34 - Asbestos inspection and removal T5-3.1.4-45 CSR 4 - No objectionable odors T5-3.1.5-45 CSR 11-5.2-Standby plans for emergency episodes T5-3.1.6-WV Code 22-5-4 (a) (14) - Annual emission inventory reporting $T5-3.1.7-40\ CFR\ Part\ 82\ Subpart\ F-Ozone\ depleting\ substances\ T5-3.1.8-40\ CFR\ Part\ 68-Risk\ Management\ Plances\ Plan$ T5-3.1.10-45 CSR 30-12.7 - Odor Control for Mercaptan T5-3.1.10-45 CSR 30-12.7 - Emergency Operating Conditions / unit replacement T5 - 3.1.12 - 45 CFR Subpart OOOOa - Reduce GHG(in the form of a limitation of Methane) and VOC emissions T5-3.3.1-45 CSR 22-5-4(a)(14-15) & 45CSR13 - Stack Testing - Conduct stack testing as required T5-3.4.1-45 CSR 30-5.1 - Monitoring information - general monitoring requirements T5 - 3.4.2 - 45 CSR 30-5.1 - Retention of records - Maintain records for a period of 5 years T5-3.4.3-45 CSR 30-5.1 - Odors - Maintain records of odor complaints and corrective actions T5-3.4.4-45 CSR 17.3-Fugitive PM shall not cause statutory Air Pollution T5-3.5.1-45 CSR 30-4.4. and 5.1.c.3.D - All documents required by permit shall be certified by a Responsible Official T5-3.5.2-45 CSR 30-5.1.c.3.E. - A permittee may request confidential treatment T5-3.5.3-45 CSR 30-5 - Communication required or permitted to be made to the DEP and/or USEPA T5 - 3.5.4 - 45 CSR 30-8 - Certified emissions statement - Operator will Submit a certified emissions statement and pay fees on an annual basis T5 - 3.5.5 - 45 CSR 30-5.3.e. - Compliance certification. The permittee shall certify compliance with the conditions of this permit on the forms provided by the DAQ T5 - 3.5.6 - 45 SR§30-5.1.c.3.A - Semi-annual monitoring reports. T5 - 3.5.7 - 45 CSR 30-5.7.a through e. - Emergencies T5-3.5.8-45 CSR 30-5.1.c.3.B. and C. - Deviations T5-3.5.9-45 CSR 30-4.3.h.1.B. New applicable requirements. If any requirement is promulgated, the permittee will meet such requirements on a timely basis

T5-3.5.10-45 CSR 30-5.1.c.3.C. Natural Gas Use certification during Compliance Certification

Permit Shield

For all facility-wide applicable requirements listed above, provide monitoring/testing / recordkeeping / reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number and/or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

T5-3.1.3-40 CFR Part 61 and 45 CSR 34-Prior to demolition/construction buildings will be inspected for asbestos and documented accordingly

T5-3.1.4-45 CSR 4-Permittee shall maintain records of all odor complaints received

T5 - 3.1.5 - 45 CSR 11 – Upon request by the Secretary, the permittee shall prepare a standby plan

T5 – 3.1.6 – WV 22-5-4 – The permittee shall submit annual emission inventory reports

T5 - 3.1.7 - 40 CFR Part 82 Subpart F - The permittee will prohibit maintenance, service, or repair of appliances containing ozone depleting substances without persons certified pursuant to 40 CFR 82.161

T5 – 3.1.8 – 40 CFR Part 68 – Should the permittee become subject to 40 CFR Part 68, a RMP shall be submitted

T5 - 3.1.10 - 45CSR§30-12.7 For emergency situations which interrupt the critical supply of natural gas to the public, and which pose a life threatening circumstance to the customer, the permittee is allowed to temporarily replace failed engine(s). Proper notice will be provided to the WVDAQ T5 - 3.3.1 - 45 CSR 22-5-4 Stack Testing – All protocols and reports will be submitted to the WVDAQ

T5 - 3.1.12 - These requirements are independent of the closed vent system and cover requirements in §60.5411a.

- T5 3.4.1 & 3.4.2 45 CSR 30-5.1 Retention of Records Maintain records of all information required by permit for 5 yrs.
- T5-3.4.3-45 CSR 30-5.1 Odors Maintain records of all odor complaints and responses.

T5 - 3.5.1 - 45 CSR 30-4.4 and 5.1 Responsible Official - Reports, certifications, etc. shall contain a certification by the responsible official.

- T5-3.5.4-45 CSR 30-8 Certified emissions statement Operator will Submit a certified emissions statement and pay fees on an annual basis
- T5-3.5.5-45 SR§30-5.3.e Compliance Certification Prepare and submit an emission inventory as requested
- T5-3.5.6-45 CSR§30-5.1.c.3.A. Semi-annual monitoring reports.

T5 - 3.5.7 - 45 CSR30-5.7.a through e. - For reporting emergency situations, refer to Section 2.17 of this permit

T5 - 3.5.8 - 45 CSR 30-5.1.c.3.B. and C. – Deviations, In addition to required monitoring reports, the permittee shall promptly submit supplemental reports and notices of deviations / include upset conditions, cause of deviation(s) and corrective actions.

T5 - 3.5.9 - 45 CSR 30-4.3.h.1.B. New applicable requirements. If any requirement is promulgated, the permittee will meet such requirements on a timely basis

T5 - 3.5.10 - 45 CSR 30-5.1.c.3.C. During compliance certification, the facility shall certify that the facility burns natural gas in all stationary equipment except, when applicable, for emergency equipment.

Are you in compliance with all facility-wide applicable requirements? 🔽 Yes 🗌 No

If no, complete the Schedule of Compliance Form as ATTACHMENT F.

21. Active Permits/Consent Orders			
Permit or Consent Order Number	Date of Issuance MM/DD/YYYY	List any Permit Determinations that Affect the Permit <i>(if any)</i>	
R30-09900013-2016 (SM01)	12/27/2016		
R13-1856C	12/18/2017		

22. Inactive Permits/Obsolete Permit Conditions				
Permit Number	Date of Issuance	Permit Condition Number		

Section 3: Facility-Wide Emissions

23. Facility-Wide Emissions Summary [Tons per Year]		
Criteria Pollutants	Potential Emissions	
Carbon Monoxide (CO)	310.41	
Nitrogen Oxides (NO _X)	3,582.71	
Lead (Pb)	-	
Particulate Matter (PM _{2.5}) ¹	41.03	
Particulate Matter (PM ₁₀) ¹	41.03	
Total Particulate Matter (TSP)	-	
Sulfur Dioxide (SO ₂)	1.23	
Volatile Organic Compounds (VOC)	107.30	
Hazardous Air Pollutants ²	Potential Emissions	
Benzene	1.39	
Toluene	0.81	
Ethylbenzene	0.11	
Xylene	0.19	
Formaldehyde	40.11	
N-hexane	0.38	
Acetaldehyde	5.58	
Total HAPs	58.00	
Regulated Pollutants other than Criteria and HAP	Potential Emissions	
CO2e	223,126.75	
$^{1}PM_{25}$ and PM_{10} are components of TSP.		

¹*PM*_{2.5} and *PM*₁₀ are components of 1SP. ²*For HAPs that are also considered PM or VOCs, emissions should be included in both the HAPs section and the Criteria Pollutants section.*

Section 4: Insignificant Activities

24.	Insign	ificant Activities (Check all that apply)
✓	1.	Air compressors and pneumatically operated equipment, including hand tools.
	2.	Air contaminant detectors or recorders, combustion controllers or shutoffs.
Image: A state of the state	3.	Any consumer product used in the same manner as in normal consumer use, provided the use results in a duration and frequency of exposure which are not greater than those experienced by consumer, and which may include, but not be limited to, personal use items; janitorial cleaning supplies, office supplies and supplies to maintain copying equipment.
 Image: A start of the start of	4.	Bathroom/toilet vent emissions.
✓	5.	Batteries and battery charging stations, except at battery manufacturing plants.
 Image: A start of the start of	6.	Bench-scale laboratory equipment used for physical or chemical analysis, but not lab fume hoods or vents. Many lab fume hoods or vents might qualify for treatment as insignificant (depending on the applicable SIP) or be grouped together for purposes of description.
	7.	Blacksmith forges.
	8.	Boiler water treatment operations, not including cooling towers.
✓	9.	Brazing, soldering or welding equipment used as an auxiliary to the principal equipment at the source.
	10.	CO ₂ lasers, used only on metals and other materials which do not emit HAP in the process.
✓	11.	Combustion emissions from propulsion of mobile sources, except for vessel emissions from Outer Continental Shelf sources.
 ✓ 	12.	Combustion units designed and used exclusively for comfort heating that use liquid petroleum gas or natural gas as fuel.
 Image: A start of the start of	13.	Comfort air conditioning or ventilation systems not used to remove air contaminants generated by or released from specific units of equipment.
	14.	Demineralized water tanks and demineralizer vents.
	15.	Drop hammers or hydraulic presses for forging or metalworking.
	16.	Electric or steam-heated drying ovens and autoclaves, but not the emissions from the articles or substances being processed in the ovens or autoclaves or the boilers delivering the steam.
	17.	Emergency (backup) electrical generators at residential locations.
	18.	Emergency road flares.
 Image: A start of the start of	19.	Emission units which do not have any applicable requirements and which emit criteria pollutants (CO, NO_x , SO ₂ , VOC and PM) into the atmosphere at a rate of less than 1 pound per hour and less than 10,000 pounds per year aggregate total for each criteria pollutant from all emission units.
		Please specify all emission units for which this exemption applies along with the quantity of criteria pollutants emitted on an hourly and annual basis:
		SEE APPENDIX A
24.	Insign	ificant Activities (Check all that apply)
---	--------	--
 Image: A start of the start of	20.	Emission units which do not have any applicable requirements and which emit hazardous air pollutants into the atmosphere at a rate of less than 0.1 pounds per hour and less than 1,000 pounds per year aggregate total for all HAPs from all emission sources. This limitation cannot be used for any source which emits dioxin/furans nor for toxic air pollutants as per 45CSR27.
		Please specify all emission units for which this exemption applies along with the quantity of hazardous air pollutants emitted on an hourly and annual basis:
		SEE APPENDIX A
	21.	Environmental chambers not using hazardous air pollutant (HAP) gases.
	22.	Equipment on the premises of industrial and manufacturing operations used solely for the purpose of preparing food for human consumption.
	23.	Equipment used exclusively to slaughter animals, but not including other equipment at slaughterhouses, such as rendering cookers, boilers, heating plants, incinerators, and electrical power generating equipment.
 Image: A start of the start of	24.	Equipment used for quality control/assurance or inspection purposes, including sampling equipment used to withdraw materials for analysis.
	25.	Equipment used for surface coating, painting, dipping or spray operations, except those that will emit VOC or HAP.
 Image: A start of the start of	26.	Fire suppression systems.
 Image: A start of the start of	27.	Firefighting equipment and the equipment used to train firefighters.
✓	28.	Flares used solely to indicate danger to the public.
 Image: A start of the start of	29.	Fugitive emission related to movement of passenger vehicle provided the emissions are not counted for applicability purposes and any required fugitive dust control plan or its equivalent is submitted.
	30.	Hand-held applicator equipment for hot melt adhesives with no VOC in the adhesive formulation.
 Image: A start of the start of	31.	Hand-held equipment for buffing, polishing, cutting, drilling, sawing, grinding, turning or machining wood, metal or plastic.
	32.	Humidity chambers.
✓	33.	Hydraulic and hydrostatic testing equipment.
✓	34.	Indoor or outdoor kerosene heaters.
✓	35.	Internal combustion engines used for landscaping purposes.
	36.	Laser trimmers using dust collection to prevent fugitive emissions.
	37.	Laundry activities, except for dry-cleaning and steam boilers.
✓	38.	Natural gas pressure regulator vents, excluding venting at oil and gas production facilities.
	39.	Oxygen scavenging (de-aeration) of water.
	40.	Ozone generators.

24.	Insign	ificant Activities (Check all that apply)
	41.	Plant maintenance and upkeep activities (e.g., grounds-keeping, general repairs, cleaning, painting, welding, plumbing, re-tarring roofs, installing insulation, and paving parking lots) provided these activities are not conducted as part of a manufacturing process, are not related to the source's primary business activity, and not otherwise triggering a permit modification. (Cleaning and painting activities qualify if they are not subject to VOC or HAP control requirements. Asphalt batch plant owners/operators must still get a permit if otherwise requested.)
 Image: A start of the start of	42.	Portable electrical generators that can be moved by hand from one location to another. "Moved by Hand" means that it can be moved without the assistance of any motorized or non-motorized vehicle, conveyance, or device.
	43.	Process water filtration systems and demineralizers.
Image: A start of the start	44.	Repair or maintenance shop activities not related to the source's primary business activity, not including emissions from surface coating or de-greasing (solvent metal cleaning) activities, and not otherwise triggering a permit modification.
	45.	Repairs or maintenance where no structural repairs are made and where no new air pollutant emitting facilities are installed or modified.
	46.	Routing calibration and maintenance of laboratory equipment or other analytical instruments.
	47.	Salt baths using nonvolatile salts that do not result in emissions of any regulated air pollutants. Shock chambers.
	48.	Shock chambers.
	49.	Solar simulators.
✓	50.	Space heaters operating by direct heat transfer.
	51.	Steam cleaning operations.
	52.	Steam leaks.
	53.	Steam sterilizers.
 Image: A start of the start of	54.	Steam vents and safety relief valves.
	55.	Storage tanks, reservoirs, and pumping and handling equipment of any size containing soaps, vegetable oil, grease, animal fat, and nonvolatile aqueous salt solutions, provided appropriate lids and covers are utilized.
	56.	Storage tanks, vessels, and containers holding or storing liquid substances that will not emit any VOC or HAP. Exemptions for storage tanks containing petroleum liquids or other volatile organic liquids should be based on size limits such as storage tank capacity and vapor pressure of liquids stored and are not appropriate for this list.
	57.	Such other sources or activities as the Director may determine.
 Image: A start of the start of	58.	Tobacco smoking rooms and areas.
 Image: A start of the start of	59.	Vents from continuous emissions monitors and other analyzers.

25. Equipment Table

Fill out the Title V Equipment Table and provide it as ATTACHMENT D.

26. Emission Units

For each emission unit listed in the **Title V Equipment Table**, fill out and provide an **Emission Unit Form** as **ATTACHMENT E**.

For each emission unit not in compliance with an applicable requirement, fill out a **Schedule of Compliance Form** as **ATTACHMENT F**.

27. Control Devices

For each control device listed in the **Title V Equipment Table**, fill out and provide an **Air Pollution Control Device Form** as **ATTACHMENT G**.

For any control device that is required on an emission unit in order to meet a standard or limitation for which the potential pre-control device emissions of an applicable regulated air pollutant is greater than or equal to the Title V Major Source Threshold Level, refer to the **Compliance Assurance Monitoring (CAM) Form(s)** for CAM applicability. Fill out and provide these forms, if applicable, for each Pollutant Specific Emission Unit (PSEU) as **ATTACHMENT H**.

28. Certification of Truth, Accuracy and Completeness and Certification of Compliance

Note: This Certification must be signed by a responsible official. The original, signed in blue ink, must be submitted with the application. Applications without an original signed certification will be considered as incomplete.

a. Certification of Truth, Accuracy and Completeness

I certify that I am a responsible official (as defined at 45CSR§30-2.38) and am accordingly authorized to make this submission on behalf of the owners or operators of the source described in this document and its attachments. I certify under penalty of law that I have personally examined and am familiar with the statements and information submitted in this document and all its attachments. Based on my inquiry of those individuals with primary responsibility for obtaining the information, I certify that the statements and information are to the best of my knowledge and belief true, accurate, and complete. I am aware that there are significant penalties for submitting false statements and information or omitting required statements and information, including the possibility of fine and/or imprisonment.

b. Compliance Certification

Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

Responsible official (type or print)

Name: Richard Smith

Title: Operations Manager

Responsible official's signature:

Signature: Richard 2. An

(Must be signed and dated in blue ink)

Not	Note: Please check all applicable attachments included with this permit application:		
\checkmark	ATTACHMENT A: Area Map		
\checkmark	ATTACHMENT B: Plot Plan(s)		
\checkmark	ATTACHMENT C: Process Flow Diagram(s)		
\checkmark	ATTACHMENT D: Equipment Table		
1	ATTACHMENT E: Emission Unit Form(s)		
	ATTACHMENT F: Schedule of Compliance Form(s)		
	ATTACHMENT G: Air Pollution Control Device Form(s)		
	ATTACHMENT H: Compliance Assurance Monitoring (CAM) Form(s)		

All of the required forms and additional information can be found and downloaded from, the DEP website at <u>www.dep.wv.gov/daq</u>, requested by phone (304) 926-0475, and/or obtained through the mail.

General Application Forms (general_forms.wpd) Page 16 of 16 Revised - 10/1/2014 Attachment A



Attachment B



Attachment C

Attachment C Ceredo Compressor Station Process Flow Diagram



Attachment D

		AT (includes a insignific	TACHMENT D - Title V Equipment Tab all emission units at the facility except those design ant activities in Section 4, Item 24 of the General I	e aated as Forms)	
Emission Point ID ¹	Control Device ¹	Emission Unit ID ¹	Emission Unit Description	Design Capacity	Year Installed/ Modified
E01	N/A	00501*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,800 hp	1954
E02	N/A	00502*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,800 hp	1954
E03	N/A	00503*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,800 hp	1954
E04	N/A	00504*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,800 hp	1957
E05	N/A	00505*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,800 hp	1958
E06	N/A	00506*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,800 hp	1960
E07	N/A	00507*	Reciprocating Engine/Integral Compressor; Cooper-Bessemer	2,700 hp	1965
E10	N/A	00510*	Solar Titan 250 Turbine	30,399 hp	2018
G3	N/A	005G3*	Reciprocating Engine/Generator; Waukesha 3521GL	812 hp	1996
H1	N/A	HTR1*	Fuel Gas Heater; FLAMECO; Model # FAH14	0.375 MMBtu/hr	1998
BL3	N/A	BLR3*	Heating System Boiler; Hurst;	6.276 MMBtu/hr	2012
G4	N/A	005G4*	Reciprocating Engine/Generator, Waukesha VGF-P48GL	1,175 hp	2018
H3	N/A	HTR3*	PROCESS HEATER	0.6 MMBtu/hr	2018

¹For 45CSR13 permitted sources, the numbering system used for the emission points, control devices, and emission units should be consistent with the numbering system used in the 45CSR13 permit. For grandfathered sources, the numbering system should be consistent with registrations or emissions inventory previously submitted to DAQ. For emission points, control devices, and emissions units which have not been previously labeled, use the following 45CSR13 numbering system: 1S, 2S, 3S,... or other appropriate description for emission units; 1C, 2C, 3C,... or other appropriate designation for control devices; 1E, 2E, 3E, ... or other appropriate designation for emission points.

Page _____ of _____

Attachment E

АТТ	TACHMENT E - Emission Un	it Form			
Emission Unit Description					
Emission unit ID number: 005G3	Emission unit name: Reciprocating Engine/Generator	List any control devices associated with this emission unit: NA			
Provide a description of the emissio 4-cycle, lean burn	on unit (type, method of operation, d	lesign parameters, etc	.):		
Manufacturer: Waukesha	Model number: 3521GL	Serial number: NA			
Construction date: NA	Installation date: 1996	Modification date(s):		
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 812 hp	,			
Maximum Hourly Throughput: NAMaximum Annual Throughput: NAMaximum Operating Schedule 8,760			ng Schedule:		
<i>Fuel Usage Data</i> (fill out all applica	ble fields)				
Does this emission unit combust fue	el? <u>X</u> Yes No	If yes, is it?			
		Indirect Fired	X_Direct Fired		
Maximum design heat input and/or	maximum horsepower rating:	Type and Btu/hr ra	ting of burners:		
812 hp		8,000 Btu/hp-hr			
List the primary fuel type(s) and if applicable, the secondary fuel type(s). For each fuel type listed, provide the maximum hourly and annual fuel usage for each. Natural Gas 6,369 scf/hr / 55,792,440 scf/yr					
Describe each fuel expected to be u	sed during the term of the permit.				
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value		
Natural Gas	Pipeline Quality		1,020 Btu/scf		

Emissions Data			
Criteria Pollutants	Potential Emissions		
	РРН		ТРҮ
Carbon Monoxide (CO)		See Appendix A	
Nitrogen Oxides (NO _X)			
Lead (Pb)			
Particulate Matter (PM _{2.5})			
Particulate Matter (PM ₁₀)			
Total Particulate Matter (TSP)			
Sulfur Dioxide (SO ₂)			
Volatile Organic Compounds (VOC)			
Hazardous Air Pollutants	I	Potential Emissions	
	РРН		ТРҮ
	See Appendix A		
Regulated Pollutants other than	Potential Emissions		
Criteria and HAP	PPH		ТРҮ
L' (() - mother d(-) mode to colonize the m	te tiel erriggiong (in alu	J. Jatan of any stack tool	
List the method(s) used to calculate the po versions of software used, source and date	es of emission factors, et	de dates of any stack test	is conducted,
See Annendix A			

Applicable Requiremen	ts
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List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

40 C.F.R. § 63.6603(a) and Table 2d (Line 10) – Maintenance Requirements
40 C.F.R. § 63.6605 – Operating Requirements
40 C.F.R. § 63.6625(e)(5), (h), and (j) – Monitoring Requirements
40 C.F.R. § 63.6640(a) and Table 6 (Line 9) – Continuous Compliance Requirements
40 C.F.R. § 63.6660 – Recordkeeping Requirements
40 C.F.R. § 63.6665 – General Requirements/Provisions
40 C.F.R. § 60 Subpart JJJJ Standards of Performance for Stationary Spark Ignition Internal Combustion Engines (SI ICE)

✓ Permit Shield

For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

40 C.F.R. § 63.6603 (a) and Table 2d (Line 10) – Change oil and oil filter, and inspect spark plugs, hoses, and belts every 1,440 hours of operation, or annually, whichever occurs first, and replace as necessary

40 C.F.R. § 63.6605 - Must comply with all emission, operating, and work practice standards at all times.

40 C.F.R. § 63.6625(e)(5), 63.6640 and Table 6 (Line 9) - Work or Management Practices: Operate and Maintain the RICE

according to the manufacturer's instructions OR develop and follow your own maintenance plan

40 C.F.R. § 63.6625 (h) - Minimize Idle Time during Startup to not exceed 30 Minutes

40 C.F.R. § 63.6625 (j) – Oil Analysis Program in lieu of Oil change requirement in Table 2d (Line 10)

40 C.F.R. § 63.6655 (d), and (e)(3) - Keep records of maintenance conducted and operating schedule on the RICE

40 C.F.R. § 63.6660 - Records retained for five (5) years and readily available for expeditious review

40 C.F.R. § 60 Subpart JJJJ establishes emission standards for applicable SI ICE. The emergency generator (G3) is subject to the emission limits for emergency engines greater than 130 hp as required under 40CFR60 Table 1.

The emission limits are 2.0 g/hp-hr for NOx, 4.0 g/hp-hr for CO, and 1.0 g/hp-hr. The emergency generator meets these emission limits.

The engine is not certified by the manufacturer to meet the emission standards listed in 40CFR60 Subpart JJJJ. Therefore, CGT will be required to conduct performance testing.

Are you in compliance with all applicable requirements for this emission unit? ✓ Yes

___No

If no, complete the Schedule of Compliance Form as ATTACHMENT F.

Page _____ of _____

ATTACHMENT E - Emission Unit Form				
Emission Unit Description				
Emission unit ID number: 00501	ission unit ID number: 01Emission unit name: Reciprocating Engine/Integral CompressorList any control devices asso with this emission unit: NA		vices associated init:	
Provide a description of the emissi 2-cycle, lean burn	on unit (type, method of operation, d	lesign parameters, etc	.):	
Manufacturer: Cooper-Bessemer	Model number: GMWH-8	Serial number: NA		
Construction date: NA	Installation date: 1954	Modification date(s NA	5):	
Design Capacity (examples: furna	ces - tons/hr, tanks - gallons): 2,800 l	hp		
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operation 8,760	ng Schedule:	
Fuel Usage Data (fill out all applic	able fields)			
Does this emission unit combust fu	lel? <u>X</u> Yes No	If yes, is it?		
		Indirect Fired	X_Direct Fired	
Maximum design heat input and/o	r maximum horsepower rating:	Type and Btu/hr ra	ting of burners:	
2,800 hp		8,400 Btu/hp-hr		
List the primary fuel type(s) and it the maximum hourly and annual f Natural Gas 23,060 scf/hr / 202,005,600 scf/yr	f applicable, the secondary fuel type(Tuel usage for each.	s). For each fuel type	listed, provide	
Describe each fuel expected to be	used during the term of the permit.			
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value	
Natural Gas	Pipeline Quality		1,020 Btu/scf	

Emissions Data					
Criteria Pollutants	Potential Emissions				
	РРН		TPY		
Carbon Monoxide (CO)		See Appendix A			
Nitrogen Oxides (NO _X)					
Lead (Pb)					
Particulate Matter (PM _{2.5})					
Particulate Matter (PM ₁₀)					
Total Particulate Matter (TSP)					
Sulfur Dioxide (SO ₂)					
Volatile Organic Compounds (VOC)					
Hazardous Air Pollutants]	Potential Emissions			
	РРН		TPY		
		See Appendix A			
Regulated Pollutants other than	Potential Emissions				
Criteria and HAP	PPH		ТРҮ		
		d. datas of any stack to	da a a da adad		
List the method(s) used to calculate the poversions of software used, source and date	es of emission factors, et	de dates of any stack les	ts conductea,		
See Annendix A					

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

X Permit Shield

For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

ATTACHMENT E - Emission Unit Form						
Emission Unit Description						
Emission unit ID number: 00502Emission unit name: Reciprocating Engine/Integral CompressorList any control devices a with this emission unit: NA		vices associated init:				
Provide a description of the emission 2-cycle, lean burn	Provide a description of the emission unit (type, method of operation, design parameters, etc.): 2-cycle, lean burn					
Manufacturer: Cooper-Bessemer	Model number: GMWH-8	Serial number: NA				
Construction date: NA	Installation date: 1954	Modification date(s NA	3):			
Design Capacity (examples: furnad	ces - tons/hr, tanks - gallons): 2,800 h	ıp				
Maximum Hourly Throughput: NAMaximum Annual Throughput: NAMaximum Operating Sch 8,760		ng Schedule:				
Fuel Usage Data (fill out all applica	able fields)					
Does this emission unit combust fu	el? <u>X</u> Yes No	If yes, is it?				
		Indirect Fired	X_Direct Fired			
Maximum design heat input and/o	r maximum horsepower rating:	Type and Btu/hr ra	ting of burners:			
2,800 hp		8,400 Btu/hp-hr				
List the primary fuel type(s) and if applicable, the secondary fuel type(s). For each fuel type listed, provide the maximum hourly and annual fuel usage for each. Natural Gas 23,060 scf/hr / 202,005,600 scf/yr						
Describe each fuel expected to be u	sed during the term of the permit.					
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value			
Natural Gas	Pipeline Quality		1,020 Btu/scf			
		1				

Emissions Data					
Criteria Pollutants	Potential Emissions				
	РРН		TPY		
Carbon Monoxide (CO)		See Appendix A			
Nitrogen Oxides (NO _X)					
Lead (Pb)					
Particulate Matter (PM _{2.5})					
Particulate Matter (PM ₁₀)					
Total Particulate Matter (TSP)					
Sulfur Dioxide (SO ₂)					
Volatile Organic Compounds (VOC)					
Hazardous Air Pollutants]	Potential Emissions			
	РРН		TPY		
		See Appendix A			
Regulated Pollutants other than	Potential Emissions				
Criteria and HAP	PPH		ТРҮ		
		d. datas of any stack to	da a a da adad		
List the method(s) used to calculate the poversions of software used, source and date	es of emission factors, et	de dates of any stack les	ts conductea,		
See Annendix A					

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

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For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

ATTACHMENT E - Emission Unit Form						
Emission Unit Description						
Emission unit ID number: 00503	nber:Emission unit name: Reciprocating Engine/Integral CompressorList any control devices associate with this emission unit: NA		vices associated init:			
Provide a description of the emissio 2-cycle, lean burn	Provide a description of the emission unit (type, method of operation, design parameters, etc.): 2-cycle, lean burn					
Manufacturer: Cooper-Bessemer	Model number: GMWH-8	Serial number: NA				
Construction date: NA	Installation date: 1954	Modification date(s):			
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 2,800 h	np				
Maximum Hourly Throughput: NA	Maximum Hourly Throughput: NAMaximum Annual Throughput: NAMaximum Operating Sched 8,760		ng Schedule:			
Fuel Usage Data (fill out all applica	ble fields)					
Does this emission unit combust fue	el? <u>X</u> Yes No	If yes, is it?	X_Direct Fired			
Maximum design heat input and/or	maximum horsepower rating:	Type and Btu/hr ra	ting of burners:			
2,800 hp		8,400 Btu/hp-hr				
List the primary fuel type(s) and if applicable, the secondary fuel type(s). For each fuel type listed, provide the maximum hourly and annual fuel usage for each. Natural Gas 23,060 scf/hr / 202,005,600 scf/yr						
Describe each fuel expected to be us	sed during the term of the permit.					
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value			
Natural Gas	Pipeline Quality		1,020 Btu/scf			

Emissions Data		
Criteria Pollutants	Potential Emissions	
	PPH	ТРҮ
Carbon Monoxide (CO)		See Appendix A
Nitrogen Oxides (NO _X)		
Lead (Pb)		
Particulate Matter (PM _{2.5})		
Particulate Matter (PM ₁₀)		
Total Particulate Matter (TSP)		
Sulfur Dioxide (SO ₂)		
Volatile Organic Compounds (VOC)		
Hazardous Air Pollutants	Ι	Potential Emissions
	РРН	ТРҮ
	See Appendix A	
Regulated Pollutants other than	J	Potential Emissions
Criteria and HAP	РРН	ТРҮ
		le la tar eferre eterle torte conducted
List the method(s) used to calculate the poversions of software used, source and date	es of emission factors, et	ide dates of any stack tests conducted,
See Annendix A		

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

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For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

AT	FACHMENT E - Emission Uni	it Form	
Emission Unit Description			
Emission unit ID number: 00504	Emission unit name: Reciprocating Engine/Integral Compressor	List any control dev with this emission u NA	vices associated init:
Provide a description of the emissio 2-cycle, lean burn	on unit (type, method of operation, d	esign parameters, etc	.):
Manufacturer: Cooper-Bessemer	Model number: GMWH-8	Serial number: NA	
Construction date: NA	Installation date: 1957	Modification date(s):
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 2,800 h	ıp	
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operation 8,760	ng Schedule:
Fuel Usage Data (fill out all applica	ble fields)		
Does this emission unit combust fu	el? <u>X</u> Yes No	If yes, is it?	
		Indirect Fired <u>X</u> Direct Fired	
Maximum design heat input and/or maximum horsepower rating:		Type and Btu/hr rating of burners:	
2,800 hp		8,400 Btu/hp-hr	
List the primary fuel type(s) and if the maximum hourly and annual fu Natural Gas 23,060 scf/hr / 202,005,600 scf/yr	applicable, the secondary fuel type(suel usage for each.	s). For each fuel type	listed, provide
Describe each fuel expected to be u	sed during the term of the permit.	1	
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value
Natural Gas	Pipeline Quality		1,020 Btu/scf

Emissions Data		
Criteria Pollutants	Potential Emissions	
	РРН	ТРҮ
Carbon Monoxide (CO)		See Appendix A
Nitrogen Oxides (NO _X)		
Lead (Pb)		
Particulate Matter (PM _{2.5})		
Particulate Matter (PM ₁₀)		
Total Particulate Matter (TSP)		
Sulfur Dioxide (SO ₂)		
Volatile Organic Compounds (VOC)		
Hazardous Air Pollutants	P	otential Emissions
	РРН	ТРҮ
		See Appendix A
Regulated Pollutants other than	P	otential Emissions
Criteria and HAP	PPH	ТРҮ
List the method(s) used to calculate the po	otential emissions (incluc	de dates of any stack tests conducted,
versions of software used, source and date	es of emission factors, etc	с.).
See Appendix A		

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

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For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

ATT	FACHMENT E - Emission Uni	it Form	
Emission Unit Description			
Emission unit ID number: 00505	Emission unit name: Reciprocating Engine/Integral Compressor	List any control dev with this emission u NA	vices associated init:
Provide a description of the emission 2-cycle, lean burn	on unit (type, method of operation, d	esign parameters, etc	.):
Manufacturer: Cooper-Bessemer	Model number: GMWH-8	Serial number: NA	
Construction date: NA	Installation date: 1958	Modification date(s NA):
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 2,800 h	ıp	
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operation 8,760	ng Schedule:
Fuel Usage Data (fill out all applica	ble fields)		
Does this emission unit combust fu	el? <u>X</u> Yes No	If yes, is it?	
		Indirect Fired X_Direct Fired	
Maximum design heat input and/or maximum horsepower rating:		Type and Btu/hr rating of burners:	
2,800 hp		8,400 Btu/hp-hr	
List the primary fuel type(s) and if applicable, the secondary fuel type(s). For each fuel type listed, provide the maximum hourly and annual fuel usage for each. Natural Gas 23,060 scf/hr / 202,005,600 scf/yr			
Describe each fuel expected to be u	sed during the term of the permit.		
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value
Natural Gas	Pipeline Quality		1,020 Btu/scf

Emissions Data		
Criteria Pollutants	Potential Emissions	
	РРН	ТРҮ
Carbon Monoxide (CO)		See Appendix A
Nitrogen Oxides (NO _X)		
Lead (Pb)		
Particulate Matter (PM _{2.5})		
Particulate Matter (PM ₁₀)		
Total Particulate Matter (TSP)		
Sulfur Dioxide (SO ₂)		
Volatile Organic Compounds (VOC)		
Hazardous Air Pollutants	P	otential Emissions
	РРН	ТРҮ
		See Appendix A
Regulated Pollutants other than	P	otential Emissions
Criteria and HAP	PPH	ТРҮ
List the method(s) used to calculate the po	otential emissions (incluc	de dates of any stack tests conducted,
versions of software used, source and date	es of emission factors, etc	с.).
See Appendix A		

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

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For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

AT	FACHMENT E - Emission Uni	it Form	
Emission Unit Description			
Emission unit ID number: 00506	Emission unit name: Reciprocating Engine/Integral Compressor	List any control dev with this emission u NA	vices associated init:
Provide a description of the emission 2-cycle, lean burn	on unit (type, method of operation, d	esign parameters, etc	.):
Manufacturer: Cooper-Bessemer	Model number: GMWH-8	Serial number: NA	
Construction date: NA	Installation date: 1960	Modification date(s NA):
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 2,800 h	ıp	
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operation 8,760	ng Schedule:
Fuel Usage Data (fill out all applica	ble fields)		
Does this emission unit combust fu	el? <u>X</u> Yes No	If yes, is it?	
		Indirect Fired X_Direct Fired	
Maximum design heat input and/or maximum horsepower rating:		Type and Btu/hr rating of burners:	
2,800 hp		8,400 Btu/hp-hr	
List the primary fuel type(s) and if applicable, the secondary fuel type(s). For each fuel type listed, provide the maximum hourly and annual fuel usage for each. Natural Gas 23,060 scf/hr / 202,005,600 scf/yr			
Describe each fuel expected to be u	sed during the term of the permit.		
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value
Natural Gas	Pipeline Quality		1,020 Btu/scf

Emissions Data		
Criteria Pollutants	Potential Emissions	
	РРН	ТРҮ
Carbon Monoxide (CO)		See Appendix A
Nitrogen Oxides (NO _X)		
Lead (Pb)		
Particulate Matter (PM _{2.5})		
Particulate Matter (PM ₁₀)		
Total Particulate Matter (TSP)		
Sulfur Dioxide (SO ₂)		
Volatile Organic Compounds (VOC)		
Hazardous Air Pollutants	P	otential Emissions
	РРН	ТРҮ
		See Appendix A
Regulated Pollutants other than	P	otential Emissions
Criteria and HAP	PPH	ТРҮ
List the method(s) used to calculate the po	otential emissions (incluc	de dates of any stack tests conducted,
versions of software used, source and date	es of emission factors, etc	с.).
See Appendix A		

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

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For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

AT	FACHMENT E - Emission Uni	it Form	
Emission Unit Description			
Emission unit ID number: 00507	Emission unit name: Reciprocating Engine/Integral Compressor	List any control dev with this emission u NA	vices associated mit:
Provide a description of the emission 2-cycle, lean burn	on unit (type, method of operation, d	esign parameters, etc.	.):
Manufacturer: Cooper-Bessemer	Model number: 8V-250	Serial number: NA	
Construction date: NA	Installation date: 1965	Modification date(s):
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 2,700 h	ıp	
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operatin 8,760	ng Schedule:
Fuel Usage Data (fill out all applica	ble fields)	1	
Does this emission unit combust fu	el? <u>X</u> Yes No	If yes, is it?	
Maximum design heat input and/or	r maximum horsepower rating:	Type and Btu/hr rating of burners:	
2,700 hp		7,800 Btu/hp-hr	
List the primary fuel type(s) and if the maximum hourly and annual f Natural Gas 20,647 scf/hr / 180,867,720 scf/yr	applicable, the secondary fuel type(s iel usage for each.	s). For each fuel type	listed, provide
Describe each fuel expected to be u	sed during the term of the permit.		
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value
Natural Gas	Pipeline Quality		1,020 Btu/scf

Emissions Data		
Criteria Pollutants	Potential Emissions	
	PPH	TPY
Carbon Monoxide (CO)		See Appendix A
Nitrogen Oxides (NO _X)		
Lead (Pb)		
Particulate Matter (PM _{2.5})		
Particulate Matter (PM ₁₀)		
Total Particulate Matter (TSP)		
Sulfur Dioxide (SO ₂)		
Volatile Organic Compounds (VOC)		
Hazardous Air Pollutants	I	Potential Emissions
	РРН	TPY
		See Appendix A
Regulated Pollutants other than	I	Potential Emissions
Criteria and HAP	РРН	TPY
List the method(s) used to colculate the pu		
versions of software used, source and date	es of emission factors, et	tc.).
See Annendix A		
Applicable Requirements

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

According to 40 CFR 63.6590(b)(3)(i) and 40 CFR 63.6600(c), this existing, non-emergency, SI 2SLB engine > 500 hp located at a major source of HAPs does not have any requirements under 40 CFR Part 63 Subpart ZZZZ because it was constructed prior to December 12, 2002.

Therefore, there are no specific applicable requirements for this emission unit other than those to submit a certified emission statement in accordance with Title V permit condition 3.5.4 and an annual emission inventory according to Title V permit condition 3.1.6.

X Permit Shield

For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

The emission unit shall track fuel usage and hours of operation in order to quantify annual emissions from this unit.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

If no, complete the Schedule of Compliance Form as ATTACHMENT F.

ATTACHMENT E - Emission Unit Form				
Emission Unit Description				
Emission unit ID number: 00510	Emission unit name: Solar Titan 250 Turbine	List any control devices associated with this emission unit: NA		
Provide a description of the emissio	n unit (type, method of operation, de	esign parameters, etc	e.):	
TURB ENG/CENT COM #0051	0			
Manufacturer: SOLAR	Model number: MARS 100	Serial number:		
Construction date: (MM/DD/YYYY)	Installation date: (MM/DD/YYYY)	Modification date(s	5): (MM/DD/YYYY)	
/ /	10/1/2018	/ / ;		
Design Capacity (examples: furnaces - tons/hr, tanks - gallons): 30399 hp				
Maximum Hourly Throughput:	Maximum Annual Throughput:	Maximum Operating Schedule:		
NA	NA	8760		
Fuel Usage Data (fill out all applical	ble fields)	l		
Does this emission unit combust fue	!? <u>√</u> Yes No	If yes, is it?		
		Indirect Fired Direct Fired		
Maximum design heat input and/or maximum horsepower rating:		Type and Btu/hr rating of burners:		
30399 hp				
List the primary fuel type(s) and if a the maximum hourly and annual fu	applicable, the secondary fuel type(s) el usage for each.	. For each fuel type	listed, provide	
Natural gas				
Describe each fuel expected to be used during the term of the permit.				
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value	
Natural Gas	Pipeline Quality		1,020 Btu/scf	

Emissions Data			
Criteria Pollutants	Potential Emissions		
	РРН	ТРҮ	
Carbon Monoxide (CO)	See Appendix A	See Appendix A	
Nitrogen Oxides (NO _X)			
Lead (Pb)			
Particulate Matter (PM _{2.5})			
Particulate Matter (PM ₁₀)			
Total Particulate Matter (TSP)			
Sulfur Dioxide (SO ₂)			
Volatile Organic Compounds (VOC)			
Hazardous Air Pollutants	Р	otential Emissions	
	РРН	ТРҮ	
Regulated Pollutants other than	Р	otential Emissions	
Criteria and HAP	РРН	ТРҮ	
List the method(s) used to calculate versions of software used, source an See Appendix A	the potential emissions (includ nd dates of emission factors, etc	le dates of any stack tests conducted, c.).	

Applicable Requirements
List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (<i>Note: Title V permit condition numbers alone are not the underlying applicable requirements</i>). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.
40 C.F.R. § 63.6603(a) and Table 2d (Line 10) – Maintenance Requirements
40 C.F.R. § $63.6625(e)(5)$, (h), and (j) – Monitoring Requirements
40 C.F.R. § 63.6640(a) and Table 6 (Line 9) – Continuous Compliance Requirements 40 C.F.R. § 63.6660 – Recordkeeping Requirements
40 C.F.R. § 63.6665 – General Requirements/Provisions 40 C.F.R § 60 Subpart KKKK Standards of Performance for Stationary Combustion Turbines
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For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)
40 C.F.R § 60 Subpart KKKK - CT shall meet NOx emission limits of 25 ppm at 15 percent O2 or 150 ng/J of useful output (1.2 lb ($MW_{\rm b}$) CT must also some burght with either new energies of 0.2 ($M_{\rm c}$)
$\{60.4330(a)\}$ (a)(2), or (a)(5). [45CSR16, 40 C.F.R. $\{60.4330(a)(1), (a)(2), or (a)(5).$ [45CSR16, 40 C.F.R. $\{60.4330(a)\}$
Are you in compliance with all applicable requirements for this emission unit? <u>Ves</u> No
If no, complete the Schedule of Compliance Form as ATTACHMENT F .
· · ·

ATTACHMENT E - Emi in Unit Form				
Emission Unit Description				
Emission unit ID number: BLR3	Emission unit name: Heating System Boiler	List any control devices associated with this emission unit: NA		
Provide a description of the emission Heating boiler	on unit (type, method of operation, d	esign parameters, etc	.):	
Manufacturer: Hurst	Model number: NA	Serial number: NA		
Construction date: NA	Installation date: 2012	Modification date(s): NA		
Design Capacity (examples: furnac	es - tons/hr, tanks - gallons): 6.276 m	nmBtu/hr		
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operating Schedule: 8,760		
Fuel Usage Data (fill out all applicable fields)				
Does this emission unit combust fu	el? <u>X</u> Yes No	If yes, is it?		
		<u>X</u> Indirect Fired	Direct Fired	
Maximum design heat input and/or	r maximum horsepower rating:	Type and Btu/hr rating of burners:		
6.276 mmBtu/hr		6.276 mmBtu/hr		
List the primary fuel type(s) and if the maximum hourly and annual fu Natural Gas 6,153 scf/hr / 53,900,000 scf/yr	applicable, the secondary fuel type(s iel usage for each.). For each fuel type	listed, provide	
Describe each fuel expected to be u	sed during the term of the permit.			
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value	
Natural Gas	Pipeline Quality		1,020 Btu/scf	

Emissions Data		
Criteria Pollutants	Potential Emissions	
	РРН	ТРҮ
Carbon Monoxide (CO)	See Appendix A	
Nitrogen Oxides (NO _X)		
Lead (Pb)		
Particulate Matter (PM _{2.5})		
Particulate Matter (PM ₁₀)		
Total Particulate Matter (TSP)		
Sulfur Dioxide (SO ₂)		
Volatile Organic Compounds (VOC)		
Hazardous Air Pollutants	Р	Potential Emissions
	РРН	ТРҮ
		See Appendix A
Regulated Pollutants other than	P	Potential Emissions
Criteria and HAP	PPH	ТРҮ
List the method(s) used to calculate the pe	otential emissions (inclue	de dates of any stack tests conducted,
versions of software used, source and date	es of emission factors, etc	c.).
See Appendix A		

Applicable Requirements

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

45CSR34, 40 C.F.R. 63.7500(a)(1)&(3) and Table 3, Item 1 – Tune Up Requirement Work Practice 40 C.F.R. 63.7510(g) Initial Compliance Demonstration Date for New Sources. 40 C.F.R. 63.7540(a)(10) & (a)(12) Tune up Requirements and Schedule

X Permit Shield

For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

40 C.F.R. 63.7515(d) Tune up Test Frequency
40 C.F.R. 63.7555(a)(1) Record of Each Notification & Report
40 C.F.R. 63.7560 Requirement for Maintaining Records
40 C.F.R. 63.7545(e)(1)&(e)(8) Notification of Compliance Status Reporting Requirements.
40 C.F.R. 63.7550(b) & (b)(5) Report Submission – Semi Annual for Title V sources
40 C.F.R. 63.7550(c)(1), (c)(5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

If no, complete the Schedule of Compliance Form as ATTACHMENT F.

ATTACHMENT E - Emission Unit Form				
Emission Unit Description				
Emission unit ID number: HTR1	Emission unit name: Fuel Gas Heater	List any control devices associated with this emission unit: NA		
Provide a description of the emission unit (type, method of operation, design parameters, etc.): Fuel Gas Heater				
Manufacturer: FLAMECO	Model number: FAH14	Serial number: NA		
Construction date: NA	Installation date: 1998	Modification date(s): NA		
Design Capacity (examples: furnaces - tons/hr, tanks - gallons): 0.375 mmBtu/hr				

Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operatin 8,760	ng Schedule:	
<i>Fuel Usage Data</i> (fill out all applical	ble fields)			
Does this emission unit combust fue	I ? <u>X</u> Yes No	If yes, is it?		
		X Indirect Fired	Direct Fired	
Maximum design heat input and/or maximum horsepower rating: Type and		Type and Btu/hr ra	ting of burners:	
0.375 mmBtu/hr		0.375 mmBtu/hr		
List the primary fuel type(s) and if applicable, the secondary fuel type(s). For each fuel type listed, provide the maximum hourly and annual fuel usage for each. Natural Gas 343.6 scf/hr / 3,010,000 scf/yr				
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value	
Natural Gas	Pipeline Quality		1,020 Btu/scf	
Emissions Data				
Criteria Pollutants	Potential Emissions			
	РРН	TP	Y	
Carbon Monoxide (CO)	See A	ppendix A		
Nitrogen Oxides (NO_X)	_			
Lead (Pb)	-			
Particulate Matter ($PM_{2.5}$)				
Total Particulate Matter (TSP)				
Sulfur Dioxide (SO ₂)				
Volatile Organic Compounds (VOC)				
Hazardous Air Pollutants	Potentia	al Emissions		
	РРН	TP	Y	
	See A	ppendix A		

Regulated Pollutants other than	Potentia	ll Emissions
Criteria and HAP	РРН	TPY

List the method(s) used to calculate the potential emissions (include dates of any stack tests conducted, versions of software used, source and dates of emission factors, etc.).

See Appendix A

Applicable Requirements

List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

45CSR34, 40 C.F.R. 63.7500(a)(1)&(3) and Table 3, Item 1 – Tune Up Requirement Work Practice 40 C.F.R. 63.7510(e) Initial Compliance Date for Existing Sources 40 C.F.R. 63.7540(a)(10) & (a)(12) Tune up Requirements and Schedule

X Permit Shield

For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

40 C.F.R. 63.7515(d) Tune up Test Frequency
40 C.F.R. 63.7555(a)(1) Record of Each Notification & Report
40 C.F.R. 63.7560 Requirement for Maintaining Records
40 C.F.R. 63.7530 (e) & (f) Initial Compliance for Existing Source Energy Assessment Requirements
40 C.F.R. 63.7545(e)(1)&(e)(8) Notification of Compliance Status Reporting Requirements.
40 C.F.R. 63.7550(b) & (b)(5) Report Submission – Semi Annual for Title V sources
40 C.F.R. 63.7550(c)(1), (c)(5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.

Are you in compliance with all applicable requirements for this emission unit? X Yes _____No

If no, complete the Schedule of Compliance Form as ATTACHMENT F.

ATTACHMENT E - Emission Unit Form				
Emission Unit Description				
Emission unit ID number: HTR3	Emission unit name: PROCESS HEATER	List any control devices associated with this emission unit: NA		
Provide a description of the emission unit (type, method of operation, design parameters, etc.): Fuel Gas Heater				
Manufacturer:	Model number:	Serial number:		
Construction date: (MM/DD/YYYY) / /	Installation date: (MM/DD/YYYY) 1 / 1 / 2018	Modification date(s): (MM/DD/YYYY) / / ; / / / ; / /		
Design Capacity (examples: furnace 0.6 MMBtu/hr	es - tons/hr, tanks - gallons):			
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operating Schedule: 8760		
Fuel Usage Data (fill out all applical	ble fields)			
Does this emission unit combust fue	I? ✓Yes No	If yes, is it?	✓ Direct Fired	
Maximum design heat input and/or maximum horsepower rating: 0.6 MMBtu/hr		Type and Btu/hr ra	ting of burners:	
List the primary fuel type(s) and if a the maximum hourly and annual fu	applicable, the secondary fuel type(s) el usage for each.). For each fuel type	listed, provide	
Natural gas				
Describe each fuel expected to be us	ed during the term of the permit.			
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value	
Natural Gas	Pipeline Quality		1,020 Btu/scf	

1		
Potential Emissions		
РРН	ТРҮ	
See Appendix A	See Appendix A	
Р	Potential Emissions	
РРН	TPY	
Potential Emissions		
РРН	ТРҮ	
the potential emissions (includ nd dates of emission factors, etc	de dates of any stack tests conducted, c.).	
	PPH See Appendix A	

Applicable Requirements	
List all applicable requi underlying rule/regulati <i>permit condition number</i> calculated based on the this information should	rements for this emission unit. For each applicable requirement, include the on citation and/or construction permit with the condition number. (<i>Note: Title V</i> is alone are not the underlying applicable requirements). If an emission limit is type of source and design capacity or if a standard is based on a design parameter, also be included.
45CSR34, 40 C.F.R. 63.7 40 C.F.R. 63.7510(e) Initi 40 C.F.R. 63.7540(a)(10)	i00(a)(1)&(3) and Table 3, Item 1 – Tune Up Requirement Work Practice al Compliance Date for Existing Sources & (a)(12) Tune up Requirements and Schedule
For all applicable requir be used to demonstrate or citation. (Note: Eacl compliance. If there is r	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number requirement listed above must have an associated method of demonstrating ot already a required method in place, then a method must be proposed.)
For all applicable require be used to demonstrate or citation. (Note: Eacl compliance. If there is n 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7560 Requirer	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number requirement listed above must have an associated method of demonstrating not already a required method in place, then a method must be proposed.) up Test Frequency cord of Each Notification & Report nent for Maintaining Records
For all applicable require be used to demonstrate or citation. (Note: Eacl compliance. If there is a 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7560 Requirer 40 C.F.R. 63.7545(e)(1)&(c) 40 C.F.R. 63.7550(b) & (b) 40 C.F.R. 63.7550(c)(1), (c)	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number requirement listed above must have an associated method of demonstrating not already a required method in place, then a method must be proposed.) up Test Frequency cord of Each Notification & Report nent for Maintaining Records (initial Compliance for Existing Source Energy Assessment Requirements)(8) Notification of Compliance Status Reporting Requirements. 5) Report Submission – Semi Annual for Title V sources (5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.
For all applicable requires be used to demonstrate for citation. (Note: Eacl compliance. If there is a 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7550 Requires 40 C.F.R. 63.7530 (e) & (f) 40 C.F.R. 63.7545(e)(1)&(c) 40 C.F.R. 63.7550(b) & (b) 40 C.F.R. 63.7550(c)(1), (c)	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number a requirement listed above must have an associated method of demonstrating not already a required method in place, then a method must be proposed.) up Test Frequency cord of Each Notification & Report nent for Maintaining Records (initial Compliance for Existing Source Energy Assessment Requirements)(8) Notification of Compliance Status Reporting Requirements. 5) Report Submission – Semi Annual for Title V sources (5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.
For all applicable require be used to demonstrate or citation. (Note: Eacl compliance. If there is 1 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7550 Requirer 40 C.F.R. 63.7530 (e) & (f) 40 C.F.R. 63.7545(e)(1)&(c 40 C.F.R. 63.7550(b) & (b) 40 C.F.R. 63.7550(c)(1), (c	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number requirement listed above must have an associated method of demonstrating out already a required method in place, then a method must be proposed.) up Test Frequency cord of Each Notification & Report nent for Maintaining Records initial Compliance for Existing Source Energy Assessment Requirements)(8) Notification of Compliance Status Reporting Requirements. 5) Report Submission – Semi Annual for Title V sources (5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.
For all applicable requires be used to demonstrate or citation. (Note: Eacl compliance. If there is a 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7550 Requires 40 C.F.R. 63.7530 (e) & (f) 40 C.F.R. 63.7545(e)(1)&(c) 40 C.F.R. 63.7550(b) & (b) 40 C.F.R. 63.7550(c)(1), (c)	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number requirement listed above must have an associated method of demonstrating tot already a required method in place, then a method must be proposed.) up Test Frequency cord of Each Notification & Report nent for Maintaining Records initial Compliance for Existing Source Energy Assessment Requirements)(8) Notification of Compliance Status Reporting Requirements. 5) Report Submission – Semi Annual for Title V sources (5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.
For all applicable requir be used to demonstrate or citation. (Note: Eacl compliance. If there is 1 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7550 Requirer 40 C.F.R. 63.7530 (e) & (f) 40 C.F.R. 63.7545(e)(1)&(c 40 C.F.R. 63.7550(b) & (b) 40 C.F.R. 63.7550(c)(1), (c	rements listed above, provide monitoring/testing/recordkeeping/reporting which shall compliance. If the method is based on a permit or rule, include the condition number requirement listed above must have an associated method of demonstrating ot already a required method in place, then a method must be proposed.) up Test Frequency cord of Each Notification & Report nent for Maintaining Records initial Compliance for Existing Source Energy Assessment Requirements)(8) Notification of Compliance Status Reporting Requirements. 5) Report Submission – Semi Annual for Title V sources (5)(i)-(iii), (c)(xiv), and (c)(xvii) Content of compliance reports.
For all applicable requir be used to demonstrate or citation. (Note: Eacl compliance. If there is 1 40 C.F.R. 63.7515(d) Tune 40 C.F.R. 63.7555(a)(1) Re 40 C.F.R. 63.7550 Requirer 40 C.F.R. 63.7545(e)(1)&(c 40 C.F.R. 63.7545(e)(1)&(c 40 C.F.R. 63.7550(c)(1), (c	rith all applicable requirements for this emission unit? ✓ YesNo

ATTACHMENT E - Emission Unit Form				
Emission Unit Description				
Emission unit ID number: 005G4	Emission unit name: RECIP ENG/GEN #005G4	List any control devices associated with this emission unit: NA		
Provide a description of the emission	n unit (type, method of operation, de	esign parameters, etc	.):	
4-cycle, lean burn Eme	rgency Generator			
Manufacturer: WAUKESHA	Model number: VGF-P48GL	Serial number:		
Construction date: (MM/DD/YYYY) / /	Installation date: (MM/DD/YYYY) 1 / 1 / 2018	Modification date(s): (MM/DD/YYYY)		
Design Capacity (examples: furnaces - tons/hr, tanks - gallons): 1,175 hp				
Maximum Hourly Throughput: NA	Maximum Annual Throughput: NA	Maximum Operating Schedule: 8760		
<i>Fuel Usage Data</i> (fill out all applicable fields)				
Does this emission unit combust fue	l? ✓Yes No	If yes, is it?		
		Indirect Fired Direct Fired		
Maximum design heat input and/or	maximum horsepower rating:	Type and Btu/hr rating of burners:		
1,175 hp				
List the primary fuel type(s) and if a the maximum hourly and annual fu	applicable, the secondary fuel type(s) el usage for each.). For each fuel type	listed, provide	
Natural gas				
Describe each fuel expected to be used during the term of the permit.				
Fuel Type	Max. Sulfur Content	Max. Ash Content	BTU Value	
Natural Gas	Pipeline Quality		1,020 Btu/scf	

1	
Р	Potential Emissions
РРН	ТРҮ
See Appendix A	See Appendix A
Р	Potential Emissions
РРН	TPY
Р	Potential Emissions
РРН	ТРҮ
the potential emissions (includ nd dates of emission factors, etc	de dates of any stack tests conducted, c.).
	PPH See Appendix A

Applicable Requiremen	ts
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List all applicable requirements for this emission unit. For each applicable requirement, include the underlying rule/regulation citation and/or <u>construction permit</u> with the condition number. (*Note: Title V permit condition numbers alone are not the underlying applicable requirements*). If an emission limit is calculated based on the type of source and design capacity or if a standard is based on a design parameter, this information should also be included.

40 C.F.R. § 63.6603(a) and Table 2d (Line 10) – Maintenance Requirements
40 C.F.R. § 63.6605 – Operating Requirements
40 C.F.R. § 63.6625(e)(5), (h), and (j) – Monitoring Requirements
40 C.F.R. § 63.6640(a) and Table 6 (Line 9) – Continuous Compliance Requirements
40 C.F.R. § 63.6660 – Recordkeeping Requirements
40 C.F.R. § 63.6665 – General Requirements/Provisions
40 C.F.R. § 60 Subpart JJJJ Standards of Performance for Stationary Spark Ignition Internal Combustion Engines (SI ICE)

✓ Permit Shield

For all applicable requirements listed above, provide monitoring/testing/recordkeeping/reporting which shall be used to demonstrate compliance. If the method is based on a permit or rule, include the condition number or citation. (Note: Each requirement listed above must have an associated method of demonstrating compliance. If there is not already a required method in place, then a method must be proposed.)

40 C.F.R. § 63.6603 (a) and Table 2d (Line 10) – Change oil and oil filter, and inspect spark plugs, hoses, and belts every 1,440 hours of operation, or annually, whichever occurs first, and replace as necessary

40 C.F.R. § 63.6605 - Must comply with all emission, operating, and work practice standards at all times.

40 C.F.R. § 63.6625(e)(5), 63.6640 and Table 6 (Line 9) - Work or Management Practices: Operate and Maintain the RICE

according to the manufacturer's instructions OR develop and follow your own maintenance plan

40 C.F.R. § 63.6625 (h) - Minimize Idle Time during Startup to not exceed 30 Minutes

40 C.F.R. § 63.6625 (j) – Oil Analysis Program in lieu of Oil change requirement in Table 2d (Line 10)

40 C.F.R. § 63.6655 (d), and (e)(3) - Keep records of maintenance conducted and operating schedule on the RICE

40 C.F.R. § 63.6660 - Records retained for five (5) years and readily available for expeditious review

40 C.F.R. § 60 Subpart JJJJ establishes emission standards for applicable SI ICE. The emergency generator (G3) is subject to the emission limits for emergency engines greater than 130 hp as required under 40CFR60 Table 1.

The emission limits are 2.0 g/hp-hr for NOx, 4.0 g/hp-hr for CO, and 1.0 g/hp-hr. The emergency generator meets these emission limits.

The engine is not certified by the manufacturer to meet the emission standards listed in 40CFR60 Subpart JJJJ. Therefore, CGT will be required to conduct performance testing.

Are you in compliance with all applicable requirements for this emission unit? ✓ Yes

___No

If no, complete the Schedule of Compliance Form as ATTACHMENT F.

Appendix A

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Facility Total PTE

									Annı	ual Emissions	s (tpy)						
Source	Capacity	Ν	IO _x	C	:0	C	CO ₂ e PM		I ₁₀ /PM _{2.5} VOC		oc		02	CH ₂ O		Total	HAP
		lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
E01 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	247.02	491.79	17.65	35.08	3,030	12,063	1.25	4.98	3.10	12.36	1.48	0.07	1.43	5.69	2.06	8.19
E02 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	247.02	491.79	17.65	35.08	3,030	12,063	1.25	4.98	3.10	12.36	1.48	0.07	1.43	5.69	2.06	8.19
E03 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	247.02	491.79	17.65	35.08	3,030	12,063	1.25	4.98	3.10	12.36	1.48	0.07	1.43	5.69	2.06	8.19
E04 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	247.02	491.79	17.65	35.08	3,030	12,063	1.25	4.98	3.10	12.36	1.48	0.07	1.43	5.69	2.06	8.19
E05 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	247.02	491.79	17.65	35.08	3,030	12,063	1.25	4.98	3.10	12.36	1.48	0.07	1.43	5.69	2.06	8.19
E06 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	247.02	491.79	17.65	35.08	3,030	12,063	1.25	4.98	3.10	12.36	1.48	0.07	1.43	5.69	2.06	8.19
E07 - Cooper-Bessemer 8V-250 Engine	2,700 hp	297.00	591.30	17.65	39.03	2,713	10,801	1.12	4.46	2.78	11.07	1.48	0.07	1.28	5.09	1.84	7.34
G3 - Waukesha Emergency Generator	812 hp	2.44	0.61	4.31	1.08	761	190	0.06	0.02	1.63	0.41	0.37	1.16E-03	0.34	0.09	0.47	0.12
H1 - Fuel Gas Heater	0.375 MMBtu/hr	0.04	0.16	0.03	0.14	44	192	2.79E-03	0.01	2.02E-03	0.01	0.02	1.17E-03	2.76E-05	1.21E-04	6.94E-04	3.04E-03
BL3 - Heating System Boiler	6.28 MMBtu/hr	0.62	2.69	0.52	2.26	735	3,219	0.05	0.20	0.03	0.15	0.36	0.02	0.000	0.002	0.01	0.05
E10 - Solar Titan 250 Turbine	30,399 hp (32 °F)	23.84	35.67	12.06	54.65	26,074	114,203	1.47	6.44	1.38	6.03	12.71	0.70	0.16	0.69	0.23	1.00
G4 - Waukesha Emergency Generator	1,175 hp	5.18	1.30	10.36	2.59	1,064	266	0.09	0.02	2.59	0.65	0.52	1.62E-03	0.49	0.12	0.67	0.17
H3 - Process Heater	0.60 MMBtu/hr	0.06	0.26	0.05	0.22	70	308	4.47E-03	0.02	3.24E-03	0.01	0.03	1.88E-03	4.41E-05	1.93E-04	1.11E-03	4.87E-03
Equipment Leaks (fugitive emissions) ^{1,2}						905.86	3,968			0.56	2.46					0.01	0.03
Liquid Storage Tanks						1.38	6.04			0.32	1.42					4.50E-06	1.97E-05
Pneumatic Emissions						69.19	303.05			0.04	0.19				-	5.74E-04	2.51E-03
Blowdowns							21,265.28				13.19						0.17
Proposed PTE ¹		1,811.26	3,582.71	150.87	310.41	49,708.07	223,132.79	10.30	41.03	27.42	107.30	24.36	1.23	10.84	40.11	15.57	58.00

Notes: 1. Excludes fugitive emissions (compressor stations are not one of the named soure categories that include fugitive emissions).

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Facility Total HAPs Emissions

Source	Capacity	Total	HAPs	Met	hanol	Forma	ldehyde	He	kane	Ben	zene	Tol	lene	Ethylbe	enzene	Xy	lene	2,2,4-Trime	thylpentane	Acetal	dehyde
000106	Capacity	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
E01 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	2.06	8.19	0.26	1.53	1.43	5.69	0.01	0.05	0.05	0.20	0.02	0.10	2.79E-03	0.01	0.01	0.03	0.02	0.09	0.20	0.80
E02 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	2.06	8.19	0.26	1.53	1.43	5.69	0.01	0.05	0.05	0.20	0.02	0.10	2.79E-03	0.01	0.01	0.03	0.02	0.09	0.20	0.80
E03 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	2.06	8.19	0.26	1.53	1.43	5.69	0.01	0.05	0.05	0.20	0.02	0.10	2.79E-03	0.01	0.01	0.03	0.02	0.09	0.20	0.80
E04 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	2.06	8.19	0.26	1.53	1.43	5.69	0.01	0.05	0.05	0.20	0.02	0.10	2.79E-03	0.01	0.01	0.03	0.02	0.09	0.20	0.80
E05 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	2.06	8.19	0.26	1.53	1.43	5.69	0.01	0.05	0.05	0.20	0.02	0.10	2.79E-03	0.01	0.01	0.03	0.02	0.09	0.20	0.80
E06 - Cooper-Bessemer GMWH-8 Engine	2,800 hp	2.06	8.19	0.26	1.53	1.43	5.69	0.01	0.05	0.05	0.20	0.02	0.10	2.79E-03	0.01	0.01	0.03	0.02	0.09	0.20	0.80
E07 - Cooper-Bessemer 8V-250 Engine	2,700 hp	1.84	7.34	0.06	0.23	1.28	5.09	0.01	0.04	0.04	0.18	0.02	0.09	2.50E-03	0.01	0.01	0.02	0.02	0.08	0.18	0.72
G3 - Waukesha Emergency Generator	812 hp	0.47	0.12	0.02	4.06E-03	0.34	0.09	0.01	1.80E-03	2.86E-03	7.15E-04	2.65E-03	6.63E-04	2.58E-04	6.45E-05	1.20E-03	2.99E-04	1.62E-03	4.06E-04	0.05	0.01
H1 - Fuel Gas Heater	0.375 MMBtu/hr	6.94E-04	3.04E-03			2.76E-05	1.21E-04	6.62E-04	2.90E-03	7.72E-07	3.38E-06	1.25E-06	5.48E-06								-
BL3 - Heating System Boiler	6.28 MMBtu/hr	0.01	0.05			4.61E-04	2.02E-03	0.01	0.05	1.29E-05	5.66E-05	2.09E-05	9.16E-05						-		
E10 - Solar Titan 250 Turbine	30,399 hp (32 °F)	0.23	1.00			0.16	0.69		-	2.67E-03	0.01	0.03	0.13	0.01	0.03					0.01	0.04
G4 - Waukesha Emergency Generator	1,175 hp	0.67	0.17	0.02	0.01	0.49	0.12	0.01	2.52E-03	4.00E-03	9.99E-04	3.71E-03	9.27E-04	3.61E-04	9.02E-05	1.67E-03	4.18E-04	2.27E-03	5.68E-04	0.08	0.02
H3 - Process Heater	0.60 MMBtu/hr	1.11E-03	4.87E-03			4.41E-05	1.93E-04	1.06E-03	4.64E-03	1.24E-06	5.41E-06	2.00E-06	8.76E-06								-
Equipment Leaks (fugitive emissions) ^{1,2}		0.01	0.03																		
Liquid Storage Tanks		<0.01	<0.01																		
Pneumatic Emissions		5.74E-04	2.51E-03																		
Blowdowns		0.04	0.17																		
Proposed PTE ¹		15.61	58.00	1.63	9.44	10.84	40.11	0.11	0.38	0.36	1.39	0.21	0.81	0.03	0.11	0.05	0.19	0.15	0.60	1.52	5.58

Notes: 1. Excludes fugitive emissions (compressor stations are not one of the named soure categories that include fugitive emissions). Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Insignificant Sources Emissions

Ceredo Compressor Station - Insignificant Sources									
	VOCs HAPs								
Emission Sources	lb/hr	lb/year	lb/hr	lb/year					
Pneumatic Emissions	0.04	376.04	<0.01	5.03					
Produced Liquids Tanks A18, A19, and A20	0.32	2841.12	<0.01	<0.01					
Wastewater Tank A21	<0.01	#VALUE!	#VALUE!	<0.01					
Totals	0.37	#VALUE!	#VALUE!	5.03					

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 2SLB Reciprocating Compressor Engines (E01 - E06)

Horsepower	2,800	HP
Maximum Horsepower	3,080	HP
Brake Specific Fuel Consumption	8,400	Btu/Bhp-hr
Total Heat Input	23.52	MMBtu/hr
Max Heat Input	25.87	MMBtu/hr
Operating Hours	8,760	hr/yr
Natural Gas Heat Content	1,020	Btu/scf
Fuel Consumption	202.00	MMscf/yr
	25,365	scf/hr
Quantity	6	

Dellutent	Emissio	on Factor		Emission Rate	Emission Easter Reference		
Pollutant	lb/MMBtu	lb/bhp-hr	lb/hr	ton/yr (per engine)	ton/yr (6 engines)	Emission Factor Reference	
NO _x (Maximum Hourly)		8.02E-02	247.02			CGT Test	
NO _x (Average Annual)		4.01E-02		491.79	2,951	CGT Test	
CO (Maximum Hourly)		5.73E-03	17.65			CGT Test	
CO (Average Annual)		2.86E-03		35.08	210	CGT Test	
CO ₂ e	117.1		3,030	12,063	72,379	40 CFR 98 Subpart C	
PM ₁₀	0.048		1.25	4.98	29.86	AP-42 Table 3.2-1 (7/00) - 2SLB	
PM _{2.5}	0.048		1.25	4.98	29.86	AP-42 Table 3.2-1 (7/00) - 2SLB	
VOC	0.120		3.10	12.36	74.17	AP-42 Table 3.2-1 (7/00) - 2SLB	
SO ₂ (Maximum Hourly)	0.0571		1.48			20 grains S / 100 scf	
SO ₂ (Average Annual)	0.000714			0.07	0.44	0.25 grains S / 100 scf	
Methanol	0.002480		0.06	0.26	1.53	AP-42 Table 3.2-1 (7/00) - 2SLB	
Hexane	0.000445		0.01	0.05	0.28	AP-42 Table 3.2-1 (7/00) - 2SLB	
Benzene	0.001940		0.05	0.20	1.20	AP-42 Table 3.2-1 (7/00) - 2SLB	
Toluene	0.000963		0.02	0.10	0.60	AP-42 Table 3.2-1 (7/00) - 2SLB	
Ethylbenzene	0.000108		0.00	0.01	0.07	AP-42 Table 3.2-1 (7/00) - 2SLB	
Acetaldehyde	0.007760		0.20	0.80	4.80	AP-42 Table 3.2-1 (7/00) - 2SLB	
2,2,4-Trimethylpentane	0.000846		0.02	0.09	0.52	AP-42 Table 3.2-1 (7/00) - 2SLB	
Xylene	0.000268		0.01	0.03	0.17	AP-42 Table 3.2-1 (7/00) - 2SLB	
Formaldehyde	0.05520		1.43	5.69	34.12	AP-42 Table 3.2-1 (7/00) - 2SLB	
Total HAPs	0.07954		2.06	8.19	49.16	AP-42 Table 3.2-1 (7/00) - 2SLB	

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 2SLB Reciprocating Compressor Engine (E07)

Horsepower	2,700	HP
Maximum Horsepower	2,970	HP
Brake Specific Fuel Consumption	7,800	Btu/Bhp-hr
Total Heat Input	21.06	MMBtu/hr
Max Heat Input	23.17	MMBtu/hr
Operating Hours	8,760	hr/yr
Natural Gas Heat Content	1,020	Btu/scf
Fuel Consumption	180.87	MMscf/yr
	22,712	scf/hr

Dellutent	Emissio	on Factor	Emiss	sion Rate	Emission Easter Deference		
Pollutant	lb/MMBtu	lb/bhp-hr	lb/hr	ton/yr	Emission Factor Reference		
NO _x (Maximum Hourly)		1.00E-01	297.00		CGT Test		
NO _x (Average Annual)		5.00E-02		591.30	CGT Test		
CO (Maximum Hourly)		6.61E-03	19.63		CGT Test		
CO (Average Annual)		3.30E-03		39.03	CGT Test		
CO ₂ e	117.1		2,713	10,801	40 CFR 98 Subpart C		
PM ₁₀	0.048		1.12	4.46	AP-42 Table 3.2-1 (7/00) - 2SLB		
PM _{2.5}	0.048		1.12	4.46	AP-42 Table 3.2-1 (7/00) - 2SLB		
VOC	0.120		2.78	11.07	AP-42 Table 3.2-1 (7/00) - 2SLB		
SO ₂ (Maximum Hourly)	0.0571		1.32		20 grains S / 100 scf		
SO ₂ (Average Annual)	0.000714			0.07	0.25 grains S / 100 scf		
Methanol	0.002480		0.06	0.23	AP-42 Table 3.2-1 (7/00) - 2SLB		
Hexane	0.000445		0.01	0.04	AP-42 Table 3.2-1 (7/00) - 2SLB		
Benzene	0.001940		0.04	0.18	AP-42 Table 3.2-1 (7/00) - 2SLB		
Toluene	0.000963		0.02	0.09	AP-42 Table 3.2-1 (7/00) - 2SLB		
Ethylbenzene	0.000108		0.00	0.01	AP-42 Table 3.2-1 (7/00) - 2SLB		
Acetaldehyde	0.007760		0.18	0.72	AP-42 Table 3.2-1 (7/00) - 2SLB		
2,2,4-Trimethylpentane	0.000846		0.02	0.08	AP-42 Table 3.2-1 (7/00) - 2SLB		
Xylene	0.000268		0.01	0.02	AP-42 Table 3.2-1 (7/00) - 2SLB		
Formaldehyde	0.05520		1.28	5.09	AP-42 Table 3.2-1 (7/00) - 2SLB		
Total HAPs	0.07954		1.84	7.34	AP-42 Table 3.2-1 (7/00) - 2SLB		

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Waukesha 4SLB Emergency Generator (G3)

Horsepower	812	hp
Brake Specific Fuel Consumption	8,000	Btu/Bhp-hr
Total Heat Input	6.50	MMBtu/hr
Operating Hours	500	hr/yr
Natural Gas Heat Content	1,020	Btu/scf
Fuel Consumption	3.18	MMscf/yr
	6,369	scf/hr

Pollutant	Emissio	n Factor	Emiss	ion Rate	Emission Eactor Potoronco		
Fondant	lb/MMBtu	lb/bhp-hr	lb/hr	ton/yr			
NO _x		3.00E-03	2.44	0.61	R13-1856 Permit Limit		
со		5.31E-03	4.31	1.08	R13-1856 Permit Limit		
CO ₂ e	117.1		761	190	40 CFR 98 Subpart C		
PM ₁₀	0.010		0.06	0.02	AP-42 Table 3.2-2 (7/00) - 4SLB		
PM _{2.5}	0.010		0.06	0.02	AP-42 Table 3.2-2 (7/00) - 4SLB		
VOC		2.01E-03	1.63	0.41	R13-1856 Permit Limit		
SO ₂ (Maximum Hourly)	0.0571		0.37		20 grains S / 100 scf		
SO ₂ (Average Annual)	0.000714			1.16E-03	0.25 grains S / 100 scf		
Methanol	0.002500		0.02	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Hexane	0.001110		0.01	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Benzene	0.000440		0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Toluene	0.000408		0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Ethylbenzene	0.000040		0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Acetaldehyde	0.008360		0.05	0.01	AP-42 Table 3.2-2 (7/00) - 4SLB		
2,2,4-Trimethylpentane	0.000250		0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Xylene	0.000184		0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB		
Formaldehyde	0.05280		0.34	0.09	AP-42 Table 3.2-2 (7/00) - 4SLB		
Total HAPs	0.07220		0.47	0.12	AP-42 Table 3.2-2 (7/00) - 4SLB		

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Fuel Gas Heater (H1)

Heat Input	
Operating Hours	
Natural Gas Heat Content	
Fuel Consumption	

0.375 MMBtu/hr 8760 hr/yr 1020 Btu/scf 3.22 MMscf/yr 367.6 scf/hr

Dellutent	Emissio	on Factor	Emissi	on Rate	Emission Easter Deference	
Pollutant	lb/MMscf	lb/MMBtu	lb/hr	ton/yr	Emission Factor Reference	
NO _x	100	0.098	0.04	0.16	AP-42 Table 1.4-1 (7/98)	
СО	84	0.082	0.03	0.14	AP-42 Table 1.4-1 (7/98)	
CO ₂ e		117.1	44	192	40 CFR 98 Subpart C	
PM ₁₀	7.6	0.007	2.79E-03	0.01	AP-42 Table 1.4-2 (7/98)	
PM _{2.5}	7.6	0.007	2.79E-03	0.01	AP-42 Table 1.4-2 (7/98)	
VOC	5.5	0.005	2.02E-03	0.01	AP-42 Table 1.4-2 (7/98)	
SO ₂ (Maximum Hourly)		0.0571	0.02		20 grains S / 100 scf	
SO ₂ (Average Annual)		0.000714		1.17E-03	0.25 grains S / 100 scf	
Hexane	1.800	0.001765	6.62E-04	2.90E-03	AP-42 Table 1.4-3 (7/98)	
Benzene	0.002100	0.000002	0.00	3.38E-06	AP-42 Table 1.4-3 (7/98)	
Toluene	0.003400	0.000003	0.00	5.48E-06	AP-42 Table 1.4-3 (7/98)	
Formaldehyde	0.075	0.00007	2.76E-05	1.21E-04	AP-42 Table 1.4-3 (7/98)	
Total HAPs	1.89	0.00185	6.94E-04	3.04E-03	AP-42 Table 1.4-3 & 4 (7/98)	

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Heating System Boiler (BL3)

Heat Input	
Operating Hours	
Natural Gas Heat Content	
Fuel Consumption	

6.276 MMBtu/hr 8760 hr/yr 1020 Btu/scf 53.90 MMscf/yr 6152.9 scf/hr

Dellutent	Emissio	on Factor	Emiss	ion Rate		
Pollutant	lb/MMscf	lb/MMBtu	lb/hr	ton/yr	Emission Factor Reference	
NO _x	100	0.098	0.62	2.69	AP-42 Table 1.4-1 (7/98)	
СО	84	0.082	0.52	2.26	AP-42 Table 1.4-1 (7/98)	
CO ₂ e		117.1	735	3,219	40 CFR 98 Subpart C	
PM ₁₀	7.6	0.007	0.05	0.20	AP-42 Table 1.4-2 (7/98)	
PM _{2.5}	7.6	0.007	0.05	0.20	AP-42 Table 1.4-2 (7/98)	
VOC	5.5	0.005	0.03	0.15	AP-42 Table 1.4-2 (7/98)	
SO ₂ (Maximum Hourly)		0.0571	0.36		20 grains S / 100 scf	
SO ₂ (Average Annual)		0.000714		0.02	0.25 grains S / 100 scf	
Hexane	1.8	0.002	0.01	0.05	AP-42 Table 1.4-3 (7/98)	
Benzene	0.0021	2.06E-06	0.00	0.00	AP-42 Table 1.4-3 (7/98)	
Toluene	0.0034	3.33E-06	0.00	0.00	AP-42 Table 1.4-3 (7/98)	
Formaldehyde	0.075	7.35E-05	4.61E-04	2.02E-03	AP-42 Table 1.4-3 (7/98)	
Total HAPs	1.89	0.00185	0.01	0.05	AP-42 Table 1.4-3 & 4 (7/98)	

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Solar Titan 250 Turbine (E10)

Horsepower Brake Specific Fuel Consumption Total Heat Input

Operating Hours Natural Gas Heat Content Fuel Consumption 30,399 hp (32 °F) 6,599 Btu/bhp-hr (LHV, 32 °F) 200.60 MMBtu/hr (LHV, 32 °F) 222.67 MMBtu/hr (HHV, 32 °F)³ 8760 hr/yr 1020 Btu/scf 1,912.31 MMscf/yr 218,300.0 scf/hr (based on 32 °F)

Dellutent	Emission Factor			Emissio	on Rate	Emission Easter Deference	
Pollutant	ppmvd@15%O2	lb/MMBt	tu	lb/hr ¹	ton/yr ²	Emission Factor Reference	
NO _x	10.00	0.039	LHV	7.93	35.67	Vendor Data	
со	25.00	0.060	LHV	12.06	54.65	Vendor Data	
GHG (CO ₂ e)		117.1	HHV	26,074	114,203	40 CFR 98 Subpart C	
PM ₁₀		0.0066	HHV	1.47	6.44	AP-42 Table 3.1-2a (4/00)	
PM _{2.5}		0.0066	HHV	1.47	6.44	AP-42 Table 3.1-2a (4/00)	
VOC	5.00	0.007	LHV	1.38	6.03	Vendor Data (20% of UHC) ⁴	
SO ₂ (Maximum Hourly)		0.0571	HHV	12.71		20 grains S / 100 scf	
SO ₂ (Average Annual)		0.000714	HHV		0.70	0.25 grains S / 100 scf	
Benzene		0.000012	HHV	0.00	0.01	AP-42 Table 3.1-3 (4/00)	
Toluene		0.000130	HHV	0.03	0.13	AP-42 Table 3.1-3 (4/00)	
Ethylbenzene		0.000032	HHV	0.01	0.03	AP-42 Table 3.1-3 (4/00)	
Acetaldehyde		0.000040	HHV	0.01	0.04	AP-42 Table 3.1-3 (4/00)	
Formaldehyde		0.00071	HHV	0.16	0.69	AP-42 Table 3.1-3 (4/00)	
Total HAPs		0.00102	HHV	0.23	1.00	AP-42 Table 3.1-3 (4/00)	

1. Maximum hourly emission rate based on normal operation at 32 °F. Heat input, fuel consumption, and emissions increase as temperature decreases, and for the purpose of this application, hourly emissions are characterized by Solar emissions data for 32 °F.

2. Annual emission rate based on maximum of: (1) normal operation or (2) normal operation plus non-SoLoNOx operation.

3. HHV heat input based on HHV=1.11*LHV

4. VOC based on 20% of vendor data for unburned hydrocarbon.

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Solar Titan 250 (E10) - Normal and Non-SoLoNOx Emission Rates

Normal and Non-SoLoNOx Emission Rates

Operating Mode	Units	NO _x	CO	VOC
Normal Load @ 32 °F ¹	lb/hr	7.93	12.06	1.38
Normal Load @ 32 °F ²	tpy	34.20	52.02	5.96
Non-SoLoNOx Operation ³	tpy	1.47	2.63	0.06
Total Emissions per Turbine	tpy	35.67	54.65	6.03

 Based on data from Solar Titan 250 Compressor Set data sheet and the following concentrations: 11 ppm NO_x; 25 ppm CO; 5 ppm VOC

2. Based on 8760 hr/yr of normal operation.

3. Potential emissions in excess of 8760 hr/yr at normal operation that may occur when turbine operates in non-SoLoNOx mode such as during low ambient temperatures (<0 °F), low load (< 50%), and during startup and shutdown events. This annual total represents the difference between the aggregate total with non-SoLoNOx operation and 8760 hr/yr of normal operation.</p>

Emission Rates During Normal Operation (g/hp-hr)¹

Emission Point ID / Model	NO _x	CO	VOC ²	SO ₂ ³	PM ₁₀ / PM _{2.5}	CH ₂ O
E10 / Solar Titan 250	0.12	0.18	0.02	0.19	0.02	0.002

1. Based on vendor performance data; values in italics based on AP-42 emission factors.

2. VOC is based on 20 percent of unburned hydrocarbons per Solar Product Information Letter 168.

3. Conservatively based on 20 grains sulfur per 100 standard cubic feet of natural gas for maximum short-term emissions.

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Waukesha VGF-P48GL Emergency Generator (G4)

Horsepower	1,175	hp
Brake Specific Fuel Consumption	7,733	Btu/Bhp-hr
Total Heat Input	9.09	MMBtu/hr
Operating Hours	500	hr/yr
Natural Gas Heat Content	1,020	Btu/scf
Fuel Consumption	4.45	MMscf/yr
	8,908	scf/hr

Pollutant Emission Factor g/bhp-hr Ib/MMBtu		n Factor	Emissi	on Rate	Emission Eactor Poteronco	
		lb/MMBtu	lb/hr	ton/yr		
NO _x	2.00		5.18	1.30	NSPS Subpart JJJJ Limitation	
со	4.00		10.36	2.59	NSPS Subpart JJJJ Limitation	
CO ₂ e		117.1	1,064	266	40 CFR 98 Subpart C	
PM ₁₀		0.010	0.09	0.02	AP-42 Table 3.2-2 (7/00) - 4SLB	
PM _{2.5}		0.010	0.09	0.02	AP-42 Table 3.2-2 (7/00) - 4SLB	
VOC	1.00		2.59	0.65	NSPS Subpart JJJJ Limitation	
SO ₂ (Maximum Hourly)		0.0571	0.52		20 grains S / 100 scf	
SO ₂ (Average Annual)		0.000714		1.62E-03	0.25 grains S / 100 scf	
Methanol		0.002500	0.02	0.01	AP-42 Table 3.2-2 (7/00) - 4SLB	
Hexane		0.001110	0.01	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB	
Benzene		0.000440	0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB	
Toluene		0.000408	0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB	
Ethylbenzene		0.000040	0.00	0.00	AP-42 Table 3.2-2 (7/00) - 4SLB	
Acetaldehyde		0.008360	0.08	0.02	AP-42 Table 3.2-2 (7/00) - 4SLB	
2,2,4-Trimethylpentane		0.000250	0.00 0.00 AP-4		AP-42 Table 3.2-2 (7/00) - 4SLB	
Xylene		0.000184	0.00 0.00		AP-42 Table 3.2-2 (7/00) - 4SLB	
Formaldehyde	0.19		0.49 0.12		Vendor Data	
Total HAPs		0.07356	0.67	0.17	AP-42 Table 3.2-2 (7/00) - 4SLB	

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Fuel Gas Heater (H3)

Heat Input	
Operating Hours	
Natural Gas Heat Content	
Fuel Consumption	

0.60 MMBtu/hr 8760 hr/yr 1020 Btu/scf 5.15 MMscf/yr 588.2 scf/hr

Dollutont	Emissio	on Factor	Emissi	ion Rate	Emission Easter Deference	
Pollutant	lb/MMscf	lb/MMBtu	lb/hr	ton/yr	Emission Factor Reference	
NO _x	100	0.098	0.06	0.26	AP-42 Table 1.4-1 (7/98)	
СО	84	0.082	0.05	0.22	AP-42 Table 1.4-1 (7/98)	
CO ₂ e		117.1	70	308	40 CFR 98 Subpart C	
PM ₁₀	7.6	0.007	4.47E-03	0.02	AP-42 Table 1.4-2 (7/98)	
PM _{2.5}	7.6	0.007	4.47E-03	0.02	AP-42 Table 1.4-2 (7/98)	
VOC	5.5	0.005	3.24E-03	0.01	AP-42 Table 1.4-2 (7/98)	
SO ₂ (Maximum Hourly)		0.0571	0.03		20 grains S / 100 scf	
SO ₂ (Average Annual)		0.000714		1.88E-03	0.25 grains S / 100 scf	
Hexane	1.800	0.001765	1.06E-03	4.64E-03	AP-42 Table 1.4-3 (7/98)	
Benzene	0.0021	0.000002	1.24E-06	5.41E-06	AP-42 Table 1.4-3 (7/98)	
Toluene	0.0034	0.000003	2.00E-06	8.76E-06	AP-42 Table 1.4-3 (7/98)	
Formaldehyde	0.075	0.00007	4.41E-05	1.93E-04	AP-42 Table 1.4-3 (7/98)	
Total HAPs	1.89	0.00185	1.11E-03	4.87E-03	AP-42 Table 1.4-3 & 4 (7/98)	

Ceredo Compressor Station Title V Permit Application - May 2021 Fugitive Emissions from Leaks

			Enviroien Easten ³	Fugitive Emissions							
Component	Number of Components ¹	Estimated Number of	Emission Factor	Total	CH ₄ ⁴		CH₄⁵	CO2 ⁵	CO₂e ⁶	VOC ⁷	HAPs ⁸
Component	Number of components	Leaking Components ²	scf/hr / component	scf/yr	scf/yr	scf/yr	ton/yr	ton/yr	ton/yr	ton/yr	ton/yr
Compressor Service											
Valve	1027	21	14.84	2,729,966	2,372,341	11,619	50.21	0.67	1255.90	0.78	0.01
Connector	2918	59	5.59	2,889,136	2,510,659	12,296	53.14	0.71	1329.12	0.82	0.01
Open-Ended Line	12	1	17.27	151,285	131,467	644	2.78	0.04	69.60	0.04	0.00
Pressure Relief Valve	13	1	39.66	347,422	301,909	1,479	6.39	0.09	159.83	0.10	0.00
Meter	1	1	19.33	169,331	147,148	721	3.11	0.04	77.90	0.05	0.00
Other	5	1	4.1	35,916	31,211	153	0.00	0.00	0.00	0.00	0.00
Non-Compressor Service											
Valve	704	15	6.42	843,588	733,078	3,590	15.52	0.21	388.09	0.24	0.00
Connector	1437	29	5.71	1,450,568	1,260,544	6,174	26.68	0.36	667.32	0.41	0.01
Open-Ended Line	0	0	11.27	0	0	0	0.00	0.00	0.00	0.00	0.00
Pressure Relief Valve	15	1	2.01	17,608	15,301	75	0.32	0.00	8.10	0.01	0.00
Meter	2	1	2.93	25,667	22,304	109	0.47	0.01	11.81	0.01	0.00
Other	3	1	4.1	35,916	31,211	153	0.00	0.00	0.00	0.00	0.00
						Total:	158.62	2.13	3967.67	2.46	0.03

Notes:

1. Number of fugitive components per Columbia Gas Transmission facility inventory data.

Estimated number of leaking components at Ceredo utilizing a 2% component leak rate factor throughout the Columbia pipeline system obtained from fugitive leak survey results at Columbia facilities, and rounded up to the nearest integer.
 Emission factors from 40 CFR 98 Subpart W Table W-3

4. CH4 and CO2 emission rates based on 86.90 vol% CH4 and 0.43 vol% CO2 in Ceredo natural gas data

5. Conversion based on densities of GHG as provided in 40 CFR 98.233(v)

6. Based on 40 CFR 98 Subpart A Global Warming Potentials

7. Based on a 0.005084 mol ratio of VOC to methane as calculated from Ceredo gas composition data

8. Based on a 0.0000379 ratio of HAPs to methane as calculated from Ceredo gas composition data

Densities per 40 CFR 98.233(v):

CH ₄	0.0192 kg/scf
CO ₂	0.0526 kg/scf

Weight Conversion Factor

2.20462 lb/kg

Global Warming Potential per 40 CFR 98 Subpart A: 25 lb CO_2e /lb CH_4

Hours/year (leap year)

8760

Ceredo Compressor Station Title V Permit Application - May 2021 Emissions from Pneumatic Devices

Type of Natural Gas Pneumatic Device	Count	EF scf/hr	Hours	CO2 Concentration	CH4 Concentration	SCF CO2	SCF CH4	CO2 lb/hr	CH4 lb/hr	VOC lb/hr	HAPS lb/hr	CO2e lb/hr	CO2 TPY	CH4 TPY2	VOC TPYE	HAPS TPY	CO2e TPY
High-Bleed Pneumatic Devices	0	18.2	8760	0.004	0.869	0.00	0.00	<0.01	< 0.01	<0.01	<0.01	<0.01	<0.01	< 0.01	<0.01	< 0.01	< 0.01
Intermittent Bleed Pneumatic Devices	32	2.35	8760	0.004	0.869	2,803.65	572,455.49	0.04	2.77	0.04	<0.01	69.19	0.16	12.12	0.19	< 0.01	303.054
Low-Bleed Pneumatic Devices	0	1.37	8760	0.004	0.869	0.00	0.00	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	< 0.01	<0.01
					Totals:	2,803.65	572,455.49	0.04	2.77	0.04	<0.01	69.19	0.16	12.12	0.19	< 0.01	303.054

Densities per 40 CFR 98.233(v):	
Density of CO_2 at standard conditions in lb/ft^3	0.1160
Density of CH_4 at standard conditions in lb/ft^3	0.0423

- Emission factors from 40 CFR 98 Subpart W Table W-3

- CH4 and CO2 emission rates based on 86.90 vol% CH4 and 0.43 vol% CO2 in Ceredo natural gas data

- Conversion based on densities of GHG as provided in 40 CFR 98.233(v)

- Based on 40 CFR 98 Subpart A Global Warming Potentials

- Based on a 0.005084 mol ratio of VOC to methane as calculated from Ceredo gas composition data

- Based on a 0.0000379 ratio of HAPs to methane as calculated from Ceredo gas composition data

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Blowdown Emissions

Component	Emission Rate (ton/yr)							
Component	CH₄¹	CO ₂	CO ₂ e	VOC ²	HAPs ³			
Equipment Blowdowns	775.22	10.40	19390.92	12.03	0.16			
Station Emergency Shutdown	74.93	1.01	1874.36	1.16	0.01			
Blowdown, Total	850.16	11.41	21265.28	13.19	0.17			

1. CH₄ emission rates based on 86.90 vol% CH₄ in annualized Ceredo natural gas data

2. Based on a 0.005084 mol ratio of VOC to methane as calculated from Ceredo gas composition data

3. Based on a 0.0000379 ratio of HAPs to methane as calculated from Ceredo gas composition data

Ceredo Facility Wide Emergency Shutdown (ESD) PTE Emission Calculations Blowdown Emissions per Event (mscf/event): 4,074.3 Blowdown Events per Year: 1

Parameter	Gas Loss from ESD (mscf/yr)	CH₄ Gas Loss (mscf/yr)	CO ₂ Gas Loss (mscf/yr)	CH₄ Emissions (ton/yr)	CO ₂ Emissions (ton/yr)	CO ₂ e Emissions (ton/yr)	VOC Emissions (ton/yr)	HAPs Emissions (ton/yr)
ESD Emissions	4,074.3	3,540.59	17.34	74.93	1.01	1,874.36	1.16	0.005

Notes:

- Gas loss volume based on TC Energy Engineering Department calculations using estimated facility piping volume, the average suction pressure, and discharge at MAOP. This volume would also be used when reporting ESD gas loss events at Frametown to PHMSA.

Compressor Startup/Shutdown PTE Emission Calculations

Unit	Blowdown Count	Average Gas Loss per Event for Unit	Annual Gas Loss from Unit	CH₄ Gas Loss (mscf/yr)	CO ₂ Gas Loss (mscf/yr)	CH₄ Emissions (ton/yr)	CO ₂ Emissions	CO ₂ e Emissions	VOC Emissions	HAPs Emissions
	100	(insci/event)		0.000	44.70	50.55	(ton/yr)	(ton/yr)	(101/91)	
EUT - Cooper-Bessemer Givivi H-8 Engine	100	27.5	2,748	2,388	11.70	50.55	0.68	1264.33	0.78	0.01
E02 - Cooper-Bessemer GMWH-8 Engine	100	27.6	2,761	2,399	11.75	50.77	0.68	1270.04	0.79	0.01
E03 - Cooper-Bessemer GMWH-8 Engine	100	27.6	2,761	2,399	11.75	50.77	0.68	1270.04	0.79	0.01
E04 - Cooper-Bessemer GMWH-8 Engine	100	27.6	2,761	2,399	11.75	50.77	0.68	1270.04	0.79	0.01
E05 - Cooper-Bessemer GMWH-8 Engine	100	30.6	3,063	2,661	13.03	56.32	0.76	1408.88	0.87	0.01
E06 - Cooper-Bessemer GMWH-8 Engine	100	30.6	3,063	2,661	13.03	56.32	0.76	1408.88	0.87	0.01
E07 - Cooper-Bessemer 8V-250 Engine	100	30.6	3,063	2,661	13.03	56.32	0.76	1408.88	0.87	0.01
Electric Unit 10 - Siemens SH712	100	27.6	2,761	2,399	11.75	50.77	0.68	1270.04	0.79	0.01
Electric Unit 11 - Siemens SH712	100	28.2	2,819	2,449	12.00	51.84	0.70	1296.68	0.80	0.01
Electric Unit 12 - Siemens SH712	100	28.2	2,819	2,449	12.00	51.84	0.70	1296.68	0.80	0.01
Electric Unit 13 - Siemens SH712	100	30.6	3,063	2,661	13.03	56.32	0.76	1408.88	0.87	0.01
E10 - Solar Titan 250 Turbine (Unit 14)	100	104.7	10,472	9,100	44.57	192.60	2.58	4817.56	2.99	0.04
Total			42,150	36,629	179.39	775.22	10.40	19,390.92	12.03	0.16

Notes:

Densities per 40 CFR 98.233(v):	
CH ₄	0.0192 kg/sct
CO ₂	0.0526 kg/sct

Weight Conversion Factor

2.20462 lb/kg

Global Warming Potential per 40 CFR 98 Subpart A:

25 lb CO2e/lb CH4

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Produced Liquids Tanks A18, A19, and A20 Insignificant Source

	Emission	Rates
Air Contaminant	Hourly	Annual
	(lb/hr)	(tpy)
VOCs	0.32	1.42
Total HAPs	<0.01	<0.01
Benzene	<0.01	<0.01
Toluene	<0.01	<0.01
Ethylbenzene	<0.01	<0.01
m-Xylene	<0.01	<0.01
n-Hexane	<0.01	<0.01
2,2,4-Trimethylpentane	<0.01	<0.01
CH ₄	0.06	0.24
CO ₂	<0.01	<0.01
CO ₂ e	1.38	6.04

Notes:

- Tank emission rates were calculated using Promax software. Promax output emissions are attached.

- Emission profiles shown above are for one (1) of the three (3) 6,000 gallon Produced Liquids Tanks. The total emissions from all 3 tanks are displayed in the emission summary tab.

Columbia Gas Transmission, LLC Ceredo Compressor Station Title V Permit Application - May 2021 Wastewater Tank A21 Insignificant Source

	Emission Rates				
Air Contaminant	Hourly (lb/hr)	Annual (tpy)			
VOCs	<0.01	<0.01			

Notes:

- Tank emission rates were calculated using Promax software. Promax output emissions are attached.

Columbia Gas Transmission, LLC Ceredo Compressor Station Natural Gas Composition

Representative Composition of Natural Gas

Natural Gas Composition	Molar Fraction ⁽¹⁾ (mole %)	Molecular Weight (lb/lb- mole)	Weighted Sum (Ib/Ib-mole)	Weight Fraction (weight %)
Nitrogen	0.51	28.01	0.1435	0.7969
Carbon Dioxide	0.43	44.01	0.1873	1.0400
Methane	86.90	16.04	13.9414	77.4075
Ethane	11.72	30.07	3.5243	19.5682
Propane	0.36	44.10	0.1567	0.8699
i-Butane	0.02	58.12	0.0125	0.0694
n-Butane	0.03	58.12	0.0194	0.1078
i-Pentane	0.01	72.15	0.0071	0.0393
n-Pentane	0.01	72.15	0.0051	0.0284
C ₆₊ Components	0.01	89.09	0.0131	0.0727
Total	100.00	-	18.01	100.00

C ₆₊ HAP Composition ⁽²⁾	Molar Fraction (mole %)	Molecular Weight (lb/lb- mole)	Weighted Sum (Ib/Ib-mole)	Weight Fraction (weight %)
2,2,4-Trimethylpentane	1.63E-04	114.23	1.86E-04	1.03E-03
Benzene	1.78E-04	78.11	1.39E-04	7.71E-04
Ethylbenzene	7.35E-06	106.17	7.80E-06	4.33E-05
n-Hexane	2.77E-03	86.18	2.39E-03	1.32E-02
Toluene	1.19E-04	92.14	1.10E-04	6.09E-04
Xylenes	5.88E-05	106.17	6.24E-05	3.47E-04
Total HAPs	3.29E-03	-	2.89E-03	1.61E-02

Totals	Mol %	Weight %
Total VOCs	0.44	1.20
Total HAPs	3.29E-03	1.60E-02

Ratios	Mol	Weight
VOC/Methane Ratio	5.08E-03	1.55E-02
HAPs/Methane Ratio	3.79E-05	2.07E-04

Mass Fraction Conversion Data

Compound	Mol Weight (g/mol)	Mass in Gas Sample (g)	Mass Fraction	Mass %
CO2	44.01	18.73	0.0104	1.0400
N2	28.02	14.35	0.0080	0.7970
Methane	16.04	1393.88	0.7739	77.3936
Ethane	30.07	352.43	0.1957	19.5683
Propane	44.09	15.67	0.0087	0.8698
I-Butane	58.12	1.25	0.0007	0.0694
N-Butane	58.12	1.94	0.0011	0.1078
I-Pentane	72.15	0.71	0.0004	0.0393
N-Pentane	72.15	0.51	0.0003	0.0284
Other hexanes	86.18	1.27	0.0007	0.0703
n-hexane	86.18	0.24	0.0001	0.0132
2,2,4 - Trimethylpentane	114.23	0.02	0.0000	0.0010
Benzene	78.11	0.01	0.0000	0.0008
Toluene	92.14	0.01	0.0000	0.0006
Ethylbenzene	106.17	0.001	0.0000	0.0000
Xylenes 106.17		0.01 0.0000		0.0003

Notes:

 $^{\left(1\right)}$ Natural gas analysis obtained from gas chromatograph readings from site data sheet.

(2) C6+ HAP composition molar fractions were derived from the GRI-GLYCALC v4.0 C6+ analysis multipliers for the Natural Gas Transmission Industry Segment.

			Pipeline Liquids Plant Schematic				
Client Name:	TCEnergy					Job: Pipeline L	iquidsA18-A20
Location:	Ceredo Compressor S	Station					
Flowsheet:	Pipeline Liquids						
		Logit Elegan, Ave 2011 El Partin Union Cases 62 Dan Banyas (2018)		TC Energy Create Compression Bartin Task AS – Add	Tan Hair' VOS + 0.0000 tory) Tan Hair' VOS + 0.0000 tory) "Wohlig Lasar' VOS + 0.0000 tory) "Wohlig Lasar' VOS + 0.0000 tory) Stading Lasar' VOS + 1.0000 tory) "Wohlig Lasar' VOS + 0.0000 tory) Tan Hair' VOS + 0.0000 tory) "Wohlig Lasar' VOS + 0.0000 tory) Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory) "Tan Hair' VOS + 0.0000 tory)	134 (b) - 0.0009 (b) - 0.000	
A18-A20_PipelineLiquids_05172021.pmx

Page 1 of 6

	Process Str All S Tabulated I	reams Report treams by Total Phase			
Client Name: TC Energy			Job: Pipel	ineLiquidsA18-A20)
Elousheet: Pipeline Liquids					
	Conn	ections			
	Breathing Losses	Gas Sample	Liquids	Liquids Sample	Loading Losses
From Block			Separator		
To Block		MIX-100	PL Liquid Tanks	MIX-100	
	Stream C	omposition			
	Breathing Losses	Gas Sample	Liquids	Liquids Sample	Loading Losses
Mole Fraction	%	%	%	%	%
Carbon Dioxide	0.207763 *	0.4256 *	0.0105828	0 *	0.207763 *
Nitrogen Methane	0.0406653 *	U.5123 * 860 *	0.012/38/	0 *	U.U406653 * 18 1803 *
Ethane	8.18678 *	11.7203 *	0.291433	0 *	8.18678 *
Propane	0.351024 *	0.3553 *	0.00883477	0 *	0.351024 *
i-Butane	0.023232 *	0.0215 *	0.000534612	0 *	0.023232 *
n-Butane	0.034668 *	0.0334 *	0.000830513	0 *	0.034668 *
n-Pentane	0.00348395	0.0098	0.000243683	0 *	0.00348395
i-Hexane	0 *	0 *	0	0 *	0 *
Heptane	0 *	0 *	0	0 *	0 *
Octane	0 *	0 *	0	0 *	0 *
Nonane	0 ^	0 *	0	0 ^	0 *
Toluene	0 *	0 *	0	0 *	0 *
Ethylbenzene	0 *	0 *	0	0 *	0 *
m-Xylene	0 *	0 *	0	0 *	0 *
n-Hexane	0.0014596 *	0.0147 *	0.000365525	0 *	0.0014596 *
	0 *	0 *	0	0 *	0 *
DecanesPlus	0 *	0 *	0	0 *	0 *
Water	0 *	0 *	0	0 *	0 *
Helium	0 *	0 *	0	0 *	0 *
Hydrogen	0 *	0 *	0	0 *	0 *
	72.9688 *	0 *	97 5134	100 *	72.9688 *
				· · ·	
	Breathing Losses	Gas Sample	Liquids	Liquids Sample	Loading
Molar Flow Carbon Dioxide	1bmol/h 6 99932E-06 *	1 7036E-05 *	1 7036F-05	Ibmol/h	1 25966E-07 *
Nitrogen	1.36997E-06 *	2.05064E-05 *	2.05064E-05	0 *	2.46552E-08 *
Methane	0.000612476 *	0.00347845 *	0.00347845	0 *	1.10226E-05 *
Ethane	0.000275804 *	0.000469142 *	0.000469142	0 *	4.96361E-06 *
Propane	1.18257E-05 *	1.4222E-05 *	1.4222E-05	0 *	2.12824E-07 *
n-Butane	1.16793F-06 *	1.33694F-06 *	1.33694F-06	0 *	2.1019F-08 *
i-Pentane	1.17371E-07 *	3.92276E-07 *	3.92276E-07	0 *	2.1123E-09 *
n-Pentane	6.21875E-08 *	2.842E-07 *	2.842E-07	0 *	1.11918E-09 *
i-Hexane	0 *	0 *	0	0 *	0 *
Heptane	0 *	0 *	0	0 *	0 *
Nonane	0 *	0 *	0	0 *	0 *
Benzene	0 *	0 *	0	0 *	0 *
Toluene	0 *	0 *	0	0 *	0 *
Ethylbenzene	0 *	0 *	0	0 *	0 *
m-Aylene			0	0 *	
2 2 4-Trimethylpentane	4.91/24E-08 "	0.00414E-U/ "	0.00414E-U/	0 *	0.04940E-10 " 0 *
Neopentane	0 *	0 *	0	0 *	0 *
DecanesPlus	0 *	0 *	0	0 *	0 *

			Process Str All S Tabulated I	reams Report treams by Total Phase			
Client Name:	TCEnergy				Job: Pipeli	neLiquidsA18-A20)
Location:	Ceredo Compres	or Station					
Flowsheet:	Pipeline Liquids						
			D 41				
Molar Flow			Breathing Losses Ibmol/h	Gas Sample Ibmol/h	Liquids Ibmol/h	Liquids Sample Ibmol/h	Loading Losses Ibmol/h
Water			0 *	0 *	0	0 *	0 *
Helium			0 *	0 *	0	0 *	0 *
Hydrogen			0 *	0 *	0	0 *	0 *
Oxygen			0 00245824 *	0 *	0 156075	0 156075 *	
LiquiusSample			0.00243824	0	0.150975	0.150975	4.424002-03
			Breathing Losses	Gas Sample	Liquids	Liquids Sample	Loading Losses
Mass Fraction			%	%	%	%	%
Carbon Dioxide			0.1118/8	1.04004 *	0.00456241	0 *	0.111878
Methane			3 56864	0.190019 77 1003 *	0.00349572	0 *	3 56864
Ethane			3.01206	19.5686 *	0.0858429	0 *	3.01206
Propane			0.189393	0.869947 *	0.00381625	0 *	0.189393
i-Butane			0.0165219	0.0693877 *	0.000304387	0 *	0.0165219
n-Butane			0.0246548	0.107793 *	0.000472862	0 *	0.0246548
i-Pentane			0.00307561	0.0392606 *	0.000172227	0 *	0.00307561
n-Pentane			0.00162958	0.0284439 *	0.000124777	0 *	0.00162958
Hentane			0	0 *	0	0 *	0
Octane			0	0 *	0	0 *	0
Nonane			0	0 *	0	0 *	0
Benzene			0	0 *	0	0 *	0
Toluene			0	0 *	0	0 *	0
Ethylbenzene			0	0 *	0	0 *	0
m-Xylene			0.00152002		0 000308565	0 *	0 00153003
2.2.4-Trimethylper	ntane		0.00133303	0.0703401	0.000300303	0 *	0.00133903
Neopentane			0	0 *	0	0 *	0
DecanesPlus			0	0 *	0	0 *	0
Water			0	0 *	0	0 *	0
Helium			0	0 *	0	0 *	0
Hydrogen			0	0 *	0	0 *	0
			93,0567	0 *	99.5613	100 *	93.0567
				-			
			Breathing Losses	Gas Sample	Liquids	Liquids Sample	Loading Losses
Mass Flow			lb/h	lb/h	lb/h	lb/h	lb/h
Carbon Dioxide			0.000308037 *	0.000749746 *	0.000749746	0 *	5.54369E-06 *
Nitrogen			3.83776E-05 *	0.000574455 *	0.000574455	0 *	6.90675E-07 *
Methane Ethano			0.00982562 *	0.0558029 *	0.0558029	0 *	0.00017683 *
Propane			0.00052146 *	0.000627129 *	0.000627129	0 *	9.38462F-06 *
i-Butane			4.54901E-05 *	5.00203E-05 *	5.00203E-05	0 *	8.18677E-07 *
n-Butane			6.78826E-05 *	7.7706E-05 *	7.7706E-05	0 *	1.22167E-06 *
i-Pentane			8.46814E-06 *	2.83023E-05 *	2.83023E-05	0 *	1.524E-07 *
n-Pentane			4.48675E-06 *	2.05047E-05 *	2.05047E-05	0 *	8.07473E-08 *
I-Hexane			0 *	0 *	0	0 *	0 *
			0 *	0 *	0	0 *	0 *
Nonane			0 *	0 *	0	0 *	0 *
Benzene			0 *	0 *	0	0 *	0 *
Toluene			0 *	0 *	0	0 *	0 *
Ethylbenzene			0 *	0 *	0	0 *	0 *
m-Xylene			0 *	0 *	0	0 *	0 *
n-Hexane	tana		4.23745E-06 *	5.07068E-05 *	5.07068E-05	0 *	7.62607E-08 *
Z,Z,4-1 IImetnylper	ilaile		0 *	U " 0 *	0	0 *	0 *
DecanesPlus			0 *	0 *	0	0 *	0 *
			·	~			

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			Process Streams Report All Streams Tabulated by Total Phase							
Client Name:	TCEnergy					Job: Pipel	ineLiquidsA18-A2	C		
Location:	Ceredo Comp	oressor Station								
Flowsheet:	Pipeline Liqui	ds								
Mass Flow			Breathing Losses Ib/h	Gas Sample Ib/h	Liq	uids p/h	Liquids Sample Ib/h	Loading Losses Ib/h		
Water			0 *	0 *		0	0 *	0 *		
Helium			0 *	0 *		0	0 *	0 *		
Hydrogen			0 *	0 *		0	0 *	0 *		
Oxygen			0 *	0 *		0	0 *	0 *		
LiquidsSample			0.256215 *	0 *		16.361	16.361 *	0.00461106 *		
			Stream	Properties						
Property		Units	Breathing Losses	Gas Sample	Liq	uids	Liquids Sample	Loading Losses		
Temperature		°F	70.3693	70 *		70	70 *	70.3693		
Pressure		psia	0.804574	564.696 *		564.696	564.696 *	0.804574		
Mole Fraction Vapo	r	%	100	100		0	0	100		
Mole Fraction Light	Liquid	%	0	0		100	100	0		
Mole Fraction Heav	y Liqui d	%	0	0		0	0	0		
Molecular Weight		lb/lbmol	81.7278	18.0093		102.083	104.227	81.7278		
Mass Density		lb/ft^3	0.0115924	1.99518		44.8369	45.0023	0.0115924		
Molar Flow		lbmol/h	0.0033689	0.00400282	0.	160978	0.156975	6.06295E-05		
Mass Flow		lb/h	0.275332	0.0720881		16.4331	16.361	0.00495511		
Vapor Volumetric Fl	OW	ft^3/h	23.7511	0.036131	0.	.366509	0.36356	0.427444		
Liquid Volumetric Fl	OW	gpm	2.96117	0.00450465	0.0	0456946	0.045327	0.0532918		
Std Vapor Volumetr	ic Flow	MMSCFD	3.06826E-05	3.64561E-05 *	0.00	0146612	0.00142967	5.5219E-07		
Std Liquid Volumetr	ric Flow	sgpm	0.000824908	0.000457651	0.0	0457651	0.0453075 *	1.48457E-05		
Compressibility			0.997218	0.896727	0.	226185	0.230087	0.997218		
Specific Gravity			2.82185	0.621816		0.7189	0.721552	2.82185		
APIGravity		.				54.0413	63.3449			
Enthalpy		Btu/h	-206.035	-134.073	-	13757.7	-13615.7	-3.70798		
Mass Enthalpy		Btu/Ib	-748.313	-1859.84	-	337.194	-832.201	-748.313		
Mass Cp		Btu/(Ib^°F)	0.375115	0.576707	0.	475266	0.473754	0.375115		
Ideal GasCpCV Rat	10	•D	1.06931	1.28373	- 0	1.05578	1.05466	1.06931		
Dynamic viscosity		CP	0.00659615	0.0116694	0.	468821	0.48919	0.00659615		
Kinematic viscosity	4		35.5218	0.365127	0.	652755	0.678613	35.5218		
	ıy		0.00847255	0.0202153	0.0	1030002	0.0637301	0.00847255		
Net Ideal Cas Hoot	ng Value	Btu/ftA2	1107 50	001 160	0.00	5128 06	0.00148828	1107 50		
Not Liquid Hosting		Btu/It	4127.00	20952 4		120.30	10000 7	4127.00		
Gross Ideal Coaller	alue		19011.0	20000.1	ļ	5500 00	10090.7 5610-10	13011.0		
Gross Liquid Hootin		Btu/It's	4400.00	22087.0		20280 0	20277 6	4430.30		
	iy value	Btu/ID	20441.1	23001.9	<u> </u>	20203.3	20211.0	20441.1		
Remarks										

emarks

			Process Str All S Tabulated I				
Client Name:	TCEnergy				Job: Pipeli	ine Liquids A18-A20)
Location:	Pipeline Liquid	essor Station					
The Wallock.		5					
			Conn	ections			
			Salas Gas	Topk Flach	Tank Liquida	Working	2
			Sales Gas	Ialik Flash		Losses	5
From Block			Separator	PL Liquid	PL Liquid		MIX-100
				Tanks	Tanks		
To Block							Separator
			Stream C	omposition			
			Sales Gas	Tank Flash	Tank Liquids	Working	3
Molo Fraction			0/	0/	0/	Losses	0/
Carbon Dioxide			/0	0.304072	0.00470991	0.207763 *	0.0105828
Nitrogen				0.60247	0.000937755	0.0406653 *	0.0127387
Methane				89.3038	0.417038	18.1803 *	2.16083
Ethane				5.66871	0.18383	8.18678 *	0.291433
Propane				0.0615534	0.00777983	0.351024 *	0.00883477
i-Butane				0.00162898	0.000512713	0.023232 *	0.000534612
i-Dulane				0.00175166	0.000812076	0.034006	0.000830513
n-Pentane				9.65651E-05	0.000178147	0.00184593 *	0.000176546
i-Hexane				0	0	0 *	0
Heptane				0	0	0 *	0
Octane				0	0	0 *	0
Nonane				0	0	0 *	0
Benzene				0	0	0 *	0
Ethylbenzene				0	0	0 *	0
m-Xvlene				0	0	0 *	0
n-Hexane				7.82807E-05	0.000371273	0.0014596 *	0.000365525
2,2,4-Trimethylpent	ane			0	0	0 *	0
Neopentane				0	0	0 *	0
DecanesPlus				0	0	0 *	0
Helium				0	0	0 *	0
Hydrogen				0	0	0 *	0
Oxygen				0	0	0 *	0
LiquidsSample				4.0557	99.3836	72.9688 *	97.5134
			Sales Gas	Tank Flash	Tank Liquids	Working Losses	3
Molar Flow			lbmol/h	Ibmol/h	lbmol/h	Ibmol/h	Ibmol/h
Carbon Dioxide			0	9.60283E-06	7.43317E-06	8.63421E-08 *	1.7036E-05
Methane			0	0.00282028	0.000658168	7.55537E-06 *	2.05064E-05
Ethane			0	0.000179022	0.00029012	3.40226E-06 *	0.000469142
Propane			0	1.9439E-06	1.22781E-05	1.45879E-07 *	1.4222E-05
i-Butane			0	5.14445E-08	8.09162E-07	9.65475E-09 *	8.60606E-07
n-Butane			0	5.53256E-08	1.28162E-06	1.44073E-08 *	1.33694E-06
I-Pentane			0	5.70164E-09	3.86575E-07	1.44786E-09 *	3.92276E-07
n-Pentane			0	3.0496E-09	2.81151E-07	1.0/131E-10 *	2.842E-07
Heptane			0	0	0	0 0 *	0
Octane			0	0	0	0 *	0
Nonane			0	0	0	0 *	0
Benzene			0	0	0	0 *	0
Toluene			0	0	0	0 *	0
Ethylbenzene			0	0	0	0 *	0
n-Hexane			0	U 2.47216F-09	U 5.85942E-07	0 ^ 6.0658E-10 *	U 5.88414F-07
2,2,4-Trimethylpent	ane		0	0	0	0 *	0
Neopentane			Ŭ Û	Ŭ,	ů 0	0 *	0
DecanesPlus			0	0	0	0 *	0

		Process Str All S Tabulated I	reams Report treams by Total Phase			
Client Name:	TCEnergy			Job: Pipeli	ineLiquidsA18-A20)
Location:	Ceredo Compressor Station					
Flowsheet:	Pipeline Liquids					
		Sales Gas	Tank Flash	Tank Liquids	Working Losses	3
Molar Flow		lbmol/h	lbmol/h	lbmol/h	lbmol/h	lbmol/h
Water		0	0	0	0 *	0
Helium		0	0	0	0 *	0
Hydrogen		0	0	0	0 *	0
Oxygen		0	0 000128082	0 156947		0 156075
LiquiusSample		0	0.000128082	0.150647	3.03243E-05	0.156975
		Sales Gas	Tank Flash	Tank Liquids	Working	3
Mass Fraction		%	%	%	Losses %	%
Carbon Dioxide			0.649925	0.00199858	0.111878	0.00456241
Nitrogen			0.819676	0.00025329	0.0139386	0.00349572
Methane			69.5795	0.0645074	3.56864	0.339576
Ethane			8.27836	0.0532966	3.01206	0.0858429
Propane			0.131822	0.00330772	0.189393	0.00381625
i-Butane			0.00459831	0.000287329	0.0165219	0.000304387
n-Butane			0.00494523	0.000455095	0.0246548	0.000472862
i-Pentane			0.000632626	0.000170398	0.00307561	0.000172227
n-Pentane			0.000338368	0.000123928	0.00162958	0.000124777
i-Hexane			0	0	0	0
Heptane			0	0	0	0
Octane			0	0	0	0
Nonane			0	0	0	0
Benzene			0	0	0	0
I oluene			0	0	0	0
Ethylbenzene			0	0	0	0
n Hovene			0 000227626	0 000208480	0.00152002	0 000208565
2.2.4 Trimothylpopt	200		0.000327626	0.000308469	0.00155905	0.000308363
2,2,4-1 Intelligipent	lane		0	0	0	0
DecanesPlus			0	0	0	0
Water			0	0	0	0
Helium			0	0	0	0
Hydrogen			0	0	0	0
Oxvgen			0	0	0	0
LiquidsSample			20.5299	99.8753	93.0567	99.5613
		Sales Gas	Tank Flash	Tank Liquids	Working	3
Mass Flow		lb/h	lb/h	lb/h	lb/h	lb/h
Carbon Dioxide		0	0.000422616	0.00032713	3.79987E-06 *	0.000749746
Nitrogen		Ŭ Û	0.000532996	4.14588E-05	4.73417E-07 *	0.000574455
Methane		0	0.0452442	0.0105586	0.000121207 *	0.0558029
Ethane		0	0.00538303	0.00872363	0.000102303 *	0.0141067
Propane		0	8.57177E-05	0.000541411	6.43261E-06 *	0.000627129
i-Butane		0	2.99007E-06	4.70302E-05	5.61155E-07 *	5.00203E-05
n-Butane		0	3.21565E-06	7.44903E-05	8.37385E-07 *	7.7706E-05
i-Pentane		0	4.11366E-07	2.78909E-05	1.04461E-07 *	2.83023E-05
n-Pentane		0	2.20025E-07	2.02847E-05	5.53475E-08 *	2.05047E-05
i-Hexane		0	0	0	0 *	0
Heptane		0	0	0	0 *	0
Octane		0	0	0	0 *	0
Nonane		0	0	0	0 *	0
Benzene		0	0	0	0 *	0
Ioluene		0	0	0	0 *	0
Ethylbenzene		0	0	0	0 *	0
m-Xylene		0	0	0	0 *	0
n-Hexane		0	2.1304E-07	5.04938E-05	5.22722E-08 *	5.07068E-05
2,2,4-1 rimethylpent	ane	0	0	0	0 *	0
Neopentane		0	0	0	0 *	0
DecanesPius		U	U	U	U *	U

			Process Str All St Tabulated b	eams Report Treams by Total Phase			
Client Name:	TCEnergy				Job: Pip	belineLiquidsA18-A2	0
Location:	Ceredo Comp	pressor Station					
Flowsheet:	Pipeline Liqui	ids					
			Sales Gas	Tank Flash	Tank Liquids	Working Losses	3
Mass Flow			lb/h	lb/h	lb/h	lb/h	lb/h
Water			0	0	0	0	" O
Helium			0	0	0	0	• O
Hydrogen			0	0	0	0	• O
Oxygen			0	0	0	0	" O
LiquidsSample			0	0.0133496	16.3477	0.00316061	16.361
			Stream	Properties			
Property		Units	Sales Gas	Tank Flash	Tank Liquids	Working Losses	3
Temperature		°F	70 *	70 *	70	70.3693	71.0182
Pressure		psia	564.696 *	14.6959 *	14.6959	0.804574	564.696
Mole Fraction Vapo	or	%		100	0	100	0
Mole Fraction Light	Liquid	%		0	100	0	100
Mole Fraction Heav	/y Liquid	%		0	0	0	0
Molecular Weight		lb/lbmol		20.5902	103.714	81.7278	102.083
Mass Density		lb/ft^3		0.053423	44.6913	0.0115924	44.8068
Molar Flow		lbmol/h	0	0.00315808	0.15782	4.1558E-05	0.160978
Mass Flow		lb/h	0	0.0650253	16.3681	0.00339644	16.4331
Vapor Volumetric F	low	ft/3/h	0	1.21/18	0.366248	0.292988	0.366755
Liquid Volumetric F	IOW	gpm	0	0.151752	0.0456621	0.0365284	0.0457253
Std Vapor Volumet	ric Flow	MMSCFD	0	2.87626E-05	0.00143736	3.78494E-07	0.00146612
Sta Liquid Volumeti	IC FIOW	sgpm	0	0.000371517	0.0453936	1.01759E-05	0.0457651
Complessibility				0.996461	0.00599988	0.997218	0.225903
A BL Crowity				0.710924	0.7 10000	2.02100	0.716417
Entholov		Rtu/b	0	107.054	12669.1	2.5416	127/0 7
Mass Enthalov		Btu/lb	0	-1660.19	-13000.1	-2.3410	-836 700
Mass Cn		Btu/(lb*°E)		0 /83185	0.47616	0 375115	0.475035
Ideal GasCnCv Rat	io	Dtu/(ID T)		1 25049	1 05492	1 06931	1 05567
Dynamic Viscosity	10	сP		0.0105986	0 458112	0.00659615	0 466059
Kinematic Viscosity	,	cSt		12 3851	0.639924	35 5218	0.649346
Thermal Conductivi	tv	Btu/(h*ft*°F)		0.0177798	0.0637077	0.00847255	0.0636323
Surface Tension	-,	lbf/ft		0.0.11100	0.00147242	?	0.00117197 ?
Net Ideal GasHeati	ng Value	Btu/ft^3		1117.74	5209.23	4127.53	5128.96
Net Liquid Heating	Value	Btu/Ib		20554.3	18900.7	19011.6	18907.3
Gross Ideal Gas He	ating Value	Btu/ft^3		1231.61	5586.32	4435.38	5500.89
Gross Liquid Heatin	ngValue	Btu/Ib		22653.2	20280.5	20441.1	20289.9
1	<u> </u>						
Remarks							

Simulation Initiated on 5/1	7/2021 5:16:35 PM		A18-A20_PipelineLiquids_05172021.pmx	(Page 1 of 1
	rt				
Client Name:	TCEnergy			Job: Pipeline	LiquidsA18-A20
Location:	Ceredo Compre	essor Station			
Flowsheet:	Pipeline Liquid	S			
			Energy Streams		
Energy Stream		Energy Rate	Power	From Block	To Block
Q-1		-18.3342 Btu/h	-0.00720562 hp		PL Liquid Tanks
Q-2		-7.95762 Btu/h	-0.00312746 hp		Separator
Remarks					

Simulation Initiated on 5/17	/2021 5:16:35 PM		A18-A20_Pipeline	eLiquids_05172021.pmx			Page 1 of 1			
			BI MI Mixer/Si	locks X-100 plitter Report						
Client Name:	TCEnergy				Job: Pipeli	neLiquidsA18	3-A20			
Location:	Ceredo Compres	sor Station		Modified: 1	1:22 AM, 10/1	6/2020				
Flowsheet:	Pipeline Liquids				Status: Sol	ved 5:14 PM,	5/17/2021			
	Connections									
Stream	Connectio	on Type	Other Block	Stream	Connect	ion Type	Other Block			
Gas Sample	Inle	ŧ		LiquidsSample	In	let				
3	Outl	et	Separator							
			Block P	arameters						
Pressure Drop		() psi	Fraction to Stream 3			100 %			
FlowMultiplier		100) %							
Remarks										

Simulation Initiated on 5/17	Simulation Initiated on 5/17/2021 5:16:35 PM A18-A20_Pipe						Page 1 of 1			
		PL Li _{Sep}	Bloc qui parato	cks d Tanks ^{r Report}						
Client Name:	TCEnergy				Job: Pipeli	neLiquidsA18	3-A20			
Location:	Ceredo Compressor Station				Modified: 1	0:08 AM, 8/2	5/2020			
Flowsheet:	Pipeline Liquids				Status: Sol	ved 5:14 PM,	5/17/2021			
Connections										
Stream	Connection Type	Other Block		Stream	Connect	ion Type	Other Block			
Liquids	Inlet	Separator		TankFlash	Vapor	Outlet				
TankLiquids	Light Liquid Outlet			Q-1	Ene	∍rgy				
		Block	< Par	rameters						
Pressure Drop		550 psi		Main Liquid Phase		Light L	iquid			
Mole Fraction Va	por 1.9	6181 %		Heat Duty		-18.3	3342 Btu/h			
Mole Fraction Lig	ht Liquid 98.	0382 %		Heat Release Curve T	уре	Plug	Flow			
Mole Fraction Hea	avy Liquid	0 %		Heat Release Curve Increments			10			
Remarks										

Simulation Initiated on 5/1	7/2021 5:16:35 PM		A18-A20_PipelineLi	iquids_05172021.pmx			Page 1 of 1				
Blocks Separator Separator Report											
Client Name:	TCEnergy				Job: Pipeline	PipelineLiquidsA18-A20					
Location:	Ceredo Compresso	or Station			Modified: 10	:09AM, 8/25/202	20				
Flowsheet:	Pipeline Liquids			Status: Solve	ed 5:14 PM, 5/17	/2021					
	Connections										
Stream	Connection	Туре С	Other Block	Stream	Connectio	on Type	Other Block				
3	Inlet	·	MIX-100	SalesGas	Vapor O	Jutlet					
Liquids	Light Liquid	Outlet PL	Liquid Tanks	Q-2	Ener	ду					
			Block Pa	arameters							
Pressure Drop		0	psi	Main Liquid Phase		Light Liquid					
Mole Fraction Va	apor	0	%	Heat Duty		-7.95762	Btu/h				
Mole Fraction Lig	ght Liquid	100	%	Heat Release Curve T	уре	Plug Flow	1				
Mole Fraction He	eavy Liquid	0	%	Heat Release Curve Increments		10					
Remarks											

		FI	owsheet Enviro	Environment onment1			
Client Name:	TCEnergy	•			Job: Pipeli	neLiquidsA18-A20	
Location:	Ceredo Compr	essor Station					
Flowsheet:	Pipeline Liquid	S					
		E	Invironm	ent Settings			
Number of Poynti	ngIntervals	0		Phase Tolerance		1 %	
Gibbs Excess Mo	del	77 °F		Emulsion Enabled		False	
Evaluation Tempe	erature						
Freeze Out Temp	erature	10 °F					
Threshold Differe	nce						
			Comp	onents			
Component Name		Henry's Law Component	Phase Initiator	Component Name		Henry's Law Component	Phase Initiator
Carbon Dioxide		False	False	Benzene		False	False
Nitrogen		False	False	Toluene		False	False
Methane		False	False	Ethylbenzene		False	False
Ethane		False	False	m-Xylene		False	False
Propane		False	False	n-Hexane		False	False
i-Butane		False	False	2,2,4-Trimethylpentane		False	False
n-Butane		False	False	Neopentane		False	False
i-Pentane		False	False	DecanesPlus		False	False
n-Pentane		False	False	Water		False	True
i-Hexane		False	False	Helium		False	False
Heptane		False	False	Hydrogen		False	False
Octane		False	False	Oxygen		False	False
Nonane		False	False	LiquidsSample		False	False
		Phys	ical Prop	erty Method Sets			
Liquid Molar Volume	e	COSTALD		Overall Package		Peng-Robins	on
Stability Calculation		Peng-Robins	on	VaporPackage		Peng-Robins	on
Light Liquid Packag	e	Peng-Robins	on	Heavy Liquid Package		Peng-Robins	on
Remarks							

		Er	nvironm	ents Report			
Client Name:	TCEnergy				Job: Pipeli	ineLiquidsA18-A20	
Location:	Ceredo Compre	essor Station					
		Р	roject-Wi	de Constants			
Atmospheric Pressu	re	14.6959	osia	Ideal GasReference Pre	ssure	14.6959	psia
Ideal Gas Reference	e Temperature	60	°F	Ideal GasReference Vo	ume	379.484	ft^3/lbmol
Liquid Reference Te	emperature	60	Ϋ́F				
		Envi	ronment	[Environment1]			
		E	Environm	ent Settings			
Number of Poynti	ng Intervals	0		Phase Tolerance		1 %	
Gibbs Excess Mo	del	77 °F		Emulsion Enabled		False	
Evaluation Tempe	erature						
Freeze Out Temp Threshold Differe	erature nce	10 °F					
			Com	onents			
Component Name		Henry's Law	Phase	Component Name		Henry's Law	Phase
		Component	Initiator			Component	Initiator
Carbon Dioxide		False	False	Benzene		False	False
Nitrogen		False	False	Toluene		False	False
Methane		False	False	Ethylbenzene		False	False
Ethane		False	False	m-Xylene		False	False
Propane		False	False	n-Hexane		False	False
i-Butane		False	False	2,2,4-Trimethylpentane		False	False
n-Butane		False	False	Neopentane		False	False
i-Pentane		False	False	DecanesPlus		False	False
n-Pentane		False	False	Water		False	True
i-Hexane		False	False	Helium		False	False
Heptane		False	False	Hydrogen		False	False
Octane		Faise	False	Oxygen		Faise	Faise
Nonane		Faise	Faise	LiquidsSample		Faise	Faise
		Phys	ical Prop	erty Method Sets			
Liquid Molar Volume	e	COSTALD		Overall Package		Peng-Robin	son
Stability Calculation		Peng-Robins	son	Vapor Package		Peng-Robin	son
Light Liquid Packag	e	Peng-Robins	son	Heavy Liquid Package		Peng-Robin	son
Remarks							

			Single Deca	e Oil Report anes Plus		
Client Name:	TCEnergy			Job: Pip	belineLiquidsA18-A20	
Location:	Ceredo Compre	essor Station				
			Pro	operties		
Volume Average I Point	Boiling	240.832	°F	Low Temperature Viscosity	0.441651	cP
* Molecular Weight		108.848	lb/lbmol	Temperature of High T Viscosity	210	°F
* Specific Gravity		0.7432		High Temperature Viscosity	0.256204	сР
API Gravity		58.8929		Watson K	11.9499	
Critical Temperate	ure	563.715	°F	ASTM D86 10-90% Slope		°F/%
Critical Pressure		421.397	psia	ASTM D93 Flash Point	47.9739	°F
Critical Volume		6.98262	ft^3/lbmol	? Pour Point	-22.4869	°F
Acentric Factor		0.350921		Paraffinic Fraction	56.3105	%
Carbon to Hydrog	en Ratio	5.84021		Naphthenic Fraction	29.8859	%
Refractive Index		1.41346		Aromatic Fraction	13.8037	%
Temperature of Lo Viscosity	ow T	100	°F	Ideal GasHeat Capacity	38.2665	Btu/(lbmol*°F)
Warnings ProMax:ProMax!Pro Warning:	iject!Oils!Decane PourPointcalc	esPluslPropertieslPoulation: The value	our Point of 240.832 °F fo	or Volume Average Boiling Point shoul	ld be between 340.33 °	F and 1040.33 °F.

Remarks

			Single Liquio	e Oil Report ds Sample					
Client Name:	TCEnergy				Job: Pipel	lineLiquidsA18-A20			
Location:	Ceredo Compre	essor Station							
	Properties								
Volume Average I Point	Boiling	221.237	°F	Low Temperature Visc	cosity	0.389635	сР		
* Molecular Weight		104.227	lb/lbmol	Temperature of High Viscosity	Γ	210	°F		
 Specific Gravity 		0.721862		High Temperature Vis	cosity	0.231388	сР		
API Gravity	API Gravity 64.5208 Watson K					12.1873			
Critical Temperate	ure	536.86	°F	ASTM D86 10-90% S	ope	0	°F/%		
Critical Pressure		417.121	psia	ASTM D93 Flash Poir	nt	34.4537	°F		
Critical Volume		6.79544	ft^3/lbmol	? Pour Point		-14.04	°F		
Acentric Factor		0.339064		Paraffinic Fraction		64.4262	%		
Carbon to Hydrog	en Ratio	5.57819		Naphthenic Fraction		26.0787	%		
Refractive Index		1.40218		Aromatic Fraction		9.49512	%		
Temperature of Lo Viscosity	owT	100	°F	Ideal GasHeat Capac	ity	37.6486	Btu/(lbmol*°F)		
Warnings ProMax:ProMax!Pro Warning:	oject!Oils!Liquids Pour Point calc	Sample!Properties! ulation: The value	Pour Point of 221.237 °F fo	or Volume Average Boiling Po	oint should b	be between 340.33 °	F and 1040.33 °F.		

Remarks

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		Calcu	lator Re	port				
Client Name:	TCEnergy				Job: Pipeli	neLiquidsA1	8-A20	
Location:	Ceredo Compre	essor Station						
		G	ias Solver					
		Sc	ource Cod	е				
Residual Error (for C	CV1) = LiquidsSa	mple-99						
		Calculat	ed Variab	e [CV1]				
Source Moniker	ProMax:ProM	ax!Project!Flowsheets!PipelineL	iquids!PStrea	ms!GasSample!I	Phases!Total	Properties!S	td Vapor Volumetric Flow	
Value	3.64561E-05							
Unit								
		Measured Va	riable [Liq	uidsSample]				
Source Moniker	ProMax:ProM	ax!Project!Flowsheets!PipelineL	iquids!PStrea	ms!Liquids!Phase	es!Total!Com	position!StdL	iquid Volumetric	
	Fraction!Liqui	dsSample						
value	99							
Unit								
		0-1-	or Dromer	lee		Statue: Se	lyed	
Error		SOIV				Status. SC	1	
		0.00990E-00 3.64561E-05 MMSCED	Prio	ynung ritv			0	
Lower Bound		MMSCED	Solv	er State			Active	
Upper Bound		MMSCFD	Gro			,		
Step Size		MMSCFD	Skip	Dependency Ch	eck		False	
ls Minimizer		False	Bloc	kDependencies			2	
Algorithm		Default	Rec	ycle Dependencie	es		0	
Iterations		3	Solv	er Dependencies	3		1	
Maxiterations		20						
Demoriko								
Remarks								
		Lie	uid Solve	<u>ار</u>				
				0				
Residual Error (for ((1) - 1 iquids - 2	4000		C				
		1000						
		Calculat	ad Variab	o [C)/4]				
Source Moniker	ProMax ProM		eu val lab	e [CVI]			Std Liquid Volumetric	
Source Moniker	Flow			ins:Erquius Samp				
Value	0.0453075							
Unit								
		Measureo	Variable	[l iquids]				
Source Moniker	ProMax:ProM	ax!Project!Flowsheets!PipelineL	iquids!PStrea	ms!TankLiquids!	Phases!Tota	Properties!L	auid Volumetric Flow	
Value	24000						1	
Unit								
		Solv	er Proper	ties		Status: So	lved	
Error		0.000451137	Мах	Iterations			20	
Calculated Value		0.0453075 sgpm	Wei	ghting			1	
Lower Bound		sgpm	* Solv	er State	l.		Active	
Upper Bound		sgpm	* Skip	Dependency Ch	eck		Irue	
Step Size		sgpm False	BIOC	k Dependencies	25		3	
Algorithm		Default	Solv	er Dependencies	55 5		0	
Iterations		2	001	2. 2020110000	•		v	
Remarks								
-								

		Calculator Report		
Client Name:	TCEnergy		Job: Pipeli	neLiquidsA18-A20
Location:	Ceredo Compre	ssor Station		

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			User Value	e Sets Report			
Client Name:	TCEnergy				Job: Pipeli	neLiquidsA18-A20)
Location:	Ceredo Compre	ssor Station					
			T	ank-1			
			Liser Value	[BlockReady]			
* Parameter		1		Upper Bound			
Lower Bound				* Enforce Bounds		False	
* Denementen		0.0		[ShellLength]			
Parameter		23	ft	* Enforce Bounds		False	π
Lonor Bound			i.	Entorico Boundo		1 4100	
			User Valu	e [ShellDiam]			
* Parameter		10	ft	Upper Bound			ft
Lower Bound			ft	* Enforce Bounds		False	
* Doromotor		0.03	User Value	e [BreatherVP]			ndia
LowerBound		0.03	psig	* Enforce Bounds		False	pag
			1 0				
			User Value	[BreatherVacP]			
* Parameter		-0.03	psig	Upper Bound			psig
LowerBound			psig	* Enforce Bounds		False	
				[Dame Dadised]			
Baramatar							<i>t</i> +
LowerBound			ft	* Enforce Bounds		False	п
			User Val	ue [OpPress]			
* Parameter		0	psig	Upper Bound		_	psig
LowerBound			psig	* Enforce Bounds		False	
				AvaDaroontLial			
* Parameter		50	%	Upper Bound			%
LowerBound			%	* Enforce Bounds		False	
			User Value [MaxPercentLiq]			
* Parameter		90	%	Upper Bound		Falsa	%
Lower Bound			70	Enforce Bounds		Faise	
			Llear Value	[MinPercentLig]			
* Parameter		10	%	Upper Bound			%
Lower Bound			%	* Enforce Bounds		False	
			User Valu	e [AnnNetTP]			
* Parameter		1.55684	bbl/day	Upper Bound		Falsa	bbl/day
Lower Bound			bbi/day	Enforce Bounds		1 8130	
			User Va	lue [OREff]			
* Parameter		0	%	Upper Bound			%
Lower Bound			%	* Enforce Bounds		False	
* Doromotor							°E
LowerBound		05.4	°F	* Enforce Bounds		False	ſ
Letter Bound						1 4130	
			User Valu	ue [MinAvaT]			
* Parameter		45.5	°F	UpperBound			°F
Lower Bound			°É	* Enforce Bounds		False	

* User Specified Values ? Extrapolated or Approximate Values

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		User Value	Sets Report		
	TOF			lah Dinali	
Location:	Ceredo Compre	assor Station		Job: Pipeli	ne Liquids A18-A20
Loodiion.	Coloue Compil				
		<u> </u>			
* Doromotor		User Value			٥٣
LowerBound		58.7899 °F	* Enforce Bounds		False
201101 200110			2		. aree
		User Val	ue [AvgP]		
* Parameter		14.16 psia	Upper Bound		psia
LowerBound		psia	* Enforce Bounds		False
* Parameter		1237 Btu/ft^2/day	UpperBound		Btu/ft^2/day
LowerBound		Btu/ft^2/day	* Enforce Bounds		False
		·			
		User Value [A	vgWindSpeed]		
* Parameter		4 mi/h	Upper Bound		mi/h
LowerBound		mi/n	Enforce Bounds		Faise
		User Value (MaxH	ourlyLoadingRate		
Parameter		bbl/hr	UpperBound		bbl/hr
LowerBound		bbl/hr	* Enforce Bounds		False
		User Value [S	umLiqLevelInc]		
Parameter		ft/yr	Upper Bound		ft/yr
Lower Dound		10 yi	Emolec Bounds		1 0130
		User Value	[FlashingT]		
* Parameter		70.3693 °F	Upper Bound		°F
LowerBound		°F	 * Enforce Bounds 		False
			trained Oil Free]		
* Parameter			UpperBound		%
LowerBound		%	* Enforce Bounds		False
		User Value [7	[urnoverRate]		
* Parameter		0.577925	Upper Bound		Foloo
Lower Bound			Enloice Bounds		False
		User Value []	ossSatFactor]		
* Parameter		1.45	UpperBound		
LowerBound			* Enforce Bounds		False
* Dama a tam		User Value [/	AtmPressure]		
Parameter		14.16 psia	* Enforce Bounds		psia False
Lower Bound					
		User Val	ue [TVP]		
* Parameter		13.5701 psia	Upper Bound		psia
LowerBound		psia	* Enforce Bounds		False
* Parameter		User Valu			nga
LowerBound		psia	* Enforce Bounds		False
		•			
		User Valu	ie [MinVP]		
* Parameter		12.9984 psia	Upper Bound		psia

			User Value	e Sets Report						
Client Name:	TC Energy				Job: Pipeli	neLiquidsA18-A20				
Location:	Ceredo Compre	essor Station								
			User Va	lue [MinVP]						
Lower Bound			psia	* Enforce Bounds		False				
* Paramotor		61 8044	Jser Value [/	AvgLiqSurfaceT]			٥E			
LowerBound		01.0044	°F	* Enforce Bounds		False	F			
User Value [MaxLigSurfaceT]										
* Parameter		70.3693	°F	Upper Bound			°F			
LowerBound			۴	* Enforce Bounds		False				
			Llear Value							
* Parameter		1,13896	ton/vr				ton/vr			
LowerBound			ton/yr	* Enforce Bounds		False	(01#)1			
			User Value [WorkingLosses]						
* Parameter		0.00462624	ton/yr	Upper Bound		Falso	ton/yr			
Lower Bound			ton/yi	Efficice Bounds		r aise				
	Liser Value [StandingLosses]									
* Parameter		0.375026	ton/yr	UpperBound			ton/yr			
Lower Bound			ton/yr	* Enforce Bounds		False				
* Downwater			User Value [RimSealLosses]			toolum			
LowerBound		0	ton/yr	* Enforce Bounds		False	ton/yi			
201101 20 0110										
			User Value [WithdrawalLoss]						
* Parameter		0	ton/yr	Upper Bound			ton/yr			
Lower Bound			ton/yr	* Enforce Bounds		False				
			llsor Value [l opdingl osses]						
* Parameter		0.0202479	ton/vr	Upper Bound			ton/vr			
LowerBound			ton/yr	* Enforce Bounds		False				
		User	Value [Max	HourlyLoadingLoss]						
* Parameter		0	lb/hr	Upper Bound		Falso	lb/hr			
Lower Bound			10/111	Enloice Bounds		1 4130				
			User Va	lue [PStar]						
Parameter				Upper Bound						
Lower Bound				* Enforce Bounds		False				
* Parameter		1 22022					ton/vr			
LowerBound		1.22003	ton/yr	* Enforce Bounds		False	.517.91			
			·	·						
		Us	er Value [Al	ICLoadingLosses]						
* Parameter		0.0217034	ton/yr	Upper Bound		F _1	ton/yr			
LowerBound			ion/yr	Enforce Bounds		Faise				
				MaxHI oadingl oes]						
* Parameter		0	Ib/hr	UpperBound			lb/hr			
Lower Bound			lb/hr	* Enforce Bounds		False				

		User	Value	Sets Report			
Client Name:	TC Energy	ener Clating			Job: Pipelir	neLiquidsA18-A20	1
Location:	Ceredo Compre	essor Station					
		User Val		Elashinglosses			
* Parameter		0.291171 ton/yr		UpperBound			ton/yr
Lower Bound		ton/yr		* Enforce Bounds		False	
		User Va	lue [De	ckFittingLosses]			
* Parameter		0 ton/yr		Upper Bound			ton/yr
Lower Bound		ton/yr		* Enforce Bounds		False	
* Domentar		User Va	lue [De				toolum
Parameter				VpperBound		Falco	ton/yr
Lower Bound		ton/yi		Enioice Bounds		l'aise	
		Llear V		lashing osseel			
* Parameter		0.0624978_top/yr		UpperBound			ton/vr
Lower Bound		ton/vr		* Enforce Bounds		False	toniyyi
		,					
		User \	/alue [TotalResidual1			
* Parameter		70.4651 ton/yr		UpperBound			ton/yr
Lower Bound		ton/yr		* Enforce Bounds		False	
		User V	alue [G	asMoleWeight]			
* Parameter		0.0200458 kg/mol	•	UpperBound			kg/mol
Lower Bound		kg/mol		* Enforce Bounds		False	
		User Val	ue [Vap	oReportableFrac]			
* Parameter		93.2935 %		Upper Bound			%
Lower Bound		%		 Enforce Bounds 		False	
				<u> </u>			
* Domonotor				[ReportableFrac]			0/
Parameter		99.8838 %		UpperBound		Falco	%
Lower Bound		70		Enioice Bounds		1 8130	
		Llsor Valu	o [Elas	hPaportableErac]			
* Parameter		21 4643 %	ie [rias				%
Lower Bound		<u> </u>		* Enforce Bounds		False	70
Remarks							
This User Value Se	et wasprogramma	atically generated. GUID={C	D98EEA	3-8B3E-47D7-BCC0-B760	573420A8}		
		Sum	`omnoi	pont Flow/Frac			
		Jaco	Value				
* Parameter			value				ton/vr
LowerBound		ton/yr		* Enforce Bounds		False	ton/yi
Lower Bound		ton, yr		Emoloo Boundo		1 4100	
Remarks							
ThisUser Value Se	et wasprogramma	tically generated. GUID={5	CABC249	9-2E47-44D4-A833-4F3D1	AF2547A}		
		Sum Co	mpone	nt Flow/Frac.177			
		User	Value	[CompSum]			
* Parameter		0.0138787 ton/yr		Upper Bound			ton/yr
Lower Bound		ton/yr		* Enforce Bounds		False	

	-	User Valu	le Sets Report					
Client Name:	TCEnergy			Job: Pipeli	ineLiquidsA18-A20			
Location:	Ceredo Compr	essor Station						
				1				
Remarks ThisUser Value Set	Remarks ThisUser Value Set wasprogrammatically generated. GUID={0BEE6B58-A118-4655-88B1-C3178E914D1F}							
		Sum Compo	nent Flow/Frac.178					
* Parameter		1.12508 ton/yr	UpperBound		ton/yr			
Lower Bound		ton/yr	* Enforce Bounds		False			
Remarks ThisUser Value Set	t wasprogramma	atically generated. GUID={1FCF7.	A22-53BB-4D85-B4D2-98034	1DCCEAC5}				
		Sum Compo	onent Flow/Frac.179					
		User Val	ue [CompSum]					
* Parameter		0.0202479 ton/yr	UpperBound		ton/yr			
Lower Bound		ton/yr	* Enforce Bounds		False			
		Sum Compo	nent Flow/Frac.186					
* Deremeter		User Val	ue [CompSum]					
Parameter		0.0134424 Ib/h	Upper Bound		ID/N False			
Lower Bound		10/11	Enforce Bounda		1 0.50			
Remarks ThisUser Value Set	t wasprogramma	atically generated. GUID={16314	387-EB06-407D-A4B5-D174F	⁻ 0939D1D}				
		Sum Compo	Inelit Flow/Flat.10/					
* Parameter		9.33114F-07 top/yr			ton/vr			
LowerBound		ton/yr	* Enforce Bounds		False			
Remarks ThisUser Value Set	t wasprogramma	atically generated. GUID={9AFAA	.5FF-7014-420C-88AF-1F950	D754536}				
		00						
		Sum Compo	onent Flow/Frac.188					
* Dava (User Val	ue [CompSum]					
^ Parameter		2.1304E-07 lb/h	Upper Bound		lb/h			
Lower Bouriu			Enloice Doulius					
Remarks ThisUser Value Set wasprogrammatically generated. GUID={8AF72F6D-9B6B-4084-A5B9-70157C63A6B1}								

		User Valu	e Sets Report						
Client Name:	TC Energy	o mor Station		Job: Pipeli	neLiquidsA18-A20				
Location:	Ceredo Compre	essor Station							
Sum Component Flow/Frac 189									
		Liser Valu							
* Parameter		0.00316866 lb/b	UpperBound		lb/b				
LowerBound		Ib/h	* Enforce Bounds		False				
Remarks ThisUser Value Se	Remarks ThisUser Value Set wasprogrammatically generated. GUID={9CB8D542-8D75-4E89-8AB7-442949EE109B}								
		Sum Compo	ent Flow/Frac 190						
* Parameter			Lipper Bound		lb/b				
LowerBound		Ib/h	* Enforce Bounds		False				
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={23E8E7	AB-B99D-4098-A3AE-61C1I	D7D4BA2E}					
		Sum Compoi	nent Flow/Frac.191						
		User Valu	ie [CompSum]						
* Parameter		1.856E-05 ton/yr	Upper Bound		ton/yr				
LowerBound		ton/yr	* Enforce Bounds		False				
			2						
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833	34-AB8B-4092-A4D0-1E7AE	D13AEE9}					
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833	34-AB8B-4092-A4D0-1E7AE	D13AEE9}					
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compo	34-AB8B-4092-A4D0-1E7AE	D13AEE9}					
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compor User Valu	34-AB8B-4092-A4D0-1E7AE nent Flow/Frac.192 le [CompSum]	D13AEE9}					
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compor User Valu 4.23745E-06 Ib/h	34-AB8B-4092-A4D0-1E7AE nent Flow/Frac.192 le [CompSum] Upper Bound * Enforce Bounds	D13AEE9}	Ib/h				
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h	AAB8B-4092-A4D0-1E7AE	D13AEE9}	Ib/h False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE	AAB8B-4092-A4D0-1E7AE	D13AEE9}	lb/h False				
Remarks ThisUser Value Se * Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE	34-AB8B-4092-A4D0-1E7AE nent Flow/Frac.192 [e [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151	D13AEE9}	lb/h False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={638833 Sum Compor User Valu 4.23745E-06 lb/h lb/h atically generated. GUID={51B0EE Sum Compor	AAB8B-4092-A4D0-1E7AE Thent Flow/Frac.192 The [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 Dent Flow/Frac.193	D13AEE9}	Ib/h False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu	AAB8B-4092-A4D0-1E7AE Pent Flow/Frac.192 [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 Pent Flow/Frac.193 [CompSum]	D13AEE9}	Ib/h False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se * Parameter	t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr	AAB8B-4092-A4D0-1E7AE Pent Flow/Frac.192 [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 [CompSum] [Upper Bound [Upper Bound]	D13AEE9}	Ib/h False ton/yr				
Remarks ThisUser Value Se * Parameter Lower Bound Remarks ThisUser Value Se * Parameter Lower Bound	t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr	AAB8B-4092-A4D0-1E7AE Pent Flow/Frac.192 [CompSum] UpperBound * Enforce Bounds 06-A063-4115-9274-E1D151 Pent Flow/Frac.193 [CompSum] UpperBound * Enforce Bounds	D13AEE9}	Ib/h False ton/yr False				
Remarks ThisUser Value Ser * Parameter Lower Bound Remarks ThisUser Value Ser * Parameter Lower Bound Remarks ThisUser Value Ser ThisUser Value Ser	t wasprogramma t wasprogramma t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr atically generated. GUID={55E106	AAB8B-4092-A4D0-1E7AE Dent Flow/Frac.192 [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 [CompSum] Upper Bound * Enforce Bounds [CompSum] Upper Bound * Enforce Bounds [CompSum] [Co	D13AEE9}	Ib/h False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma t wasprogramma t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr atically generated. GUID={55E106	AAB8B-4092-A4D0-1E7AE Dent Flow/Frac.192 [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 [CompSum] Upper Bound * Enforce Bounds [CompSum] Upper Bound * Enforce Bounds [CompSum] [Co	D13AEE9}	Ib/h False ton/yr False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma t wasprogramma t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr atically generated. GUID={55E106 Sum Compor	34-AB8B-4092-A4D0-1E7AE Dent Flow/Frac.192 le [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 Dent Flow/Frac.193 le [CompSum] Upper Bound * Enforce Bounds 91-B7DA-4FAA-9B9E-0B68E Dent Flow/Frac.194	D13AEE9}	Ib/h False ton/yr False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Comparison	t wasprogramma t wasprogramma t wasprogramma t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr atically generated. GUID={55E106 Sum Compor User Valu	34-AB8B-4092-A4D0-1E7AE Dent Flow/Frac.192 [e [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 [of compSum] Upper Bound * Enforce Bounds 91-B7DA-4FAA-9B9E-0B68E [of compSum] [of compSum]	D13AEE9}	Ib/h False ton/yr False				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Parameter Lower Pound	t wasprogramma t wasprogramma t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr atically generated. GUID={55E106 Sum Compor User Valu 3.34022E-07 ton/yr	AAB8B-4092-A4D0-1E7AE Pent Flow/Frac.192 [E [CompSum] Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 [CompSum] Upper Bound * Enforce Bounds 91-B7DA-4FAA-9B9E-0B68E [CompSum] Upper Bound * Enforce Bounds [E [CompSum] Upper Bound [E [CompSum] Upper Bound [E [CompSum] Upper Bound [E [CompSum] [E [C	D13AEE9}	Ib/h False ton/yr False ton/yr				
Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se Analysis Remarks ThisUser Value Se Parameter Lower Bound Remarks ThisUser Value Se	t wasprogramma t wasprogramma t wasprogramma t wasprogramma	atically generated. GUID={6388333 Sum Compor User Valu 4.23745E-06 Ib/h Ib/h atically generated. GUID={51B0EE Sum Compor User Valu 2.28952E-07 ton/yr ton/yr atically generated. GUID={55E106 Sum Compor User Valu 3.34022E-07 ton/yr ton/yr	AAB8B-4092-A4D0-1E7AE Pent Flow/Frac.192 Upper Bound * Enforce Bounds 06-A063-4115-9274-E1D151 06-A063-4115-9274-E1D151 Upper Bound * Enforce Bounds 91-B7DA-4FAA-9B9E-0B68E Pent Flow/Frac.194 Upper Bound * Enforce Bounds Physical States of the second secon	D13AEE9}	Ib/h False ton/yr False				

^{*} User Specified Values ? Extrapolated or Approximate Values

		User Valu	e Sets Report						
Client Name:	ICEnergy	eeen Chatien		Job: Pipelin	ne Liquids A18-A20				
Location:	Ceredo Compre	ssor Station		-					
ThisUser Value Set	ThisUser Value Set wasprogrammatically generated. GUID={75C56AB5-55B0-40BE-BD77-0FEA32ACB487}								
		Sum Compo	nent Flow/Frac 195						
		User Vali	ue [CompSum]						
* Parameter		0.0046228 lb/h	UpperBound		lb/h				
LowerBound		lb/h	* Enforce Bounds		False				
		Sum Compo	nent Flow/Frac.196						
		User Val	ue [CompSum]						
* Parameter		5.22722E-08 lb/h	Upper Bound		lb/h				
Lower Bound		lb/h	* Enforce Bounds		False				
Remarks ThisUser Value Set	Remarks This User Value Set was programmatically generated. GUID={CA38BC43-757A-43DF-B7AE-5B8482D705C9}								
		Sum Compo	nent Flow/Frac.197						
		User Val	ue [CompSum]						
* Parameter		7.62607E-08 lb/h	Upper Bound		lb/h				
LowerBound		lb/h	* Enforce Bounds		False				
Remarks ThisUser Value Set	wasprogramma	tically generated. GUID={D1DB1	1B0-87F0-46EA-90A6-6AC7	3B0D6340}					

Page 1 of 7

				Recoveri	es Report				
Client Name:	TCEner	gy Gamma	eren Otetien				Job: Pipeline	Liquids	A18-A20
Location:	Ceredo	Compre	essor Station						
	•		Compo	nont Pocov	orios - Proio	et Inlote	<u> </u>		Status: Solved
) Duciest		
			Recovery Stre	eam Data So	Durce - All Ir	nets in F	roject		
Flowsh	eet		PStream	n	FI	owsheet			PStream
Pipeline L	iquias		Gas Sam	pie	Pipe		15		LiquidsSample
Composition Desi	_		Malar	Parar	neters	Onter		Ctre	
Composition Bas	S		worarriow		Summation	Option		Strea	amsand
Calculate Ratios			Falso		Atomic Basi	c		Sui	False
Carculate Matios			1 4130		Atomic Das	3			1 0130
				Tabula	tod Data				
						-			
		Рір	eline Liquids:Gas	Pipeline Liq	uids:Liquids	Sur	nmary Table		
Index			Ibmol/h	San	ol/h		lbmol/b		
Carbon Dioxid	de		1.7036E-05	1.011	0		1.7036E-0)5	
Nitrogen			2.05064E-05		0		2.05064E-	05	
Methane			0.00347845		0		0.0034784	45	
Ethane			0.000469142		0		0.00046914	42	
Propane			1.4222E-05		0		1.4222E-0)5	
i-Butane			8.60606E-07		0		8.60606E-0	07	
n-Butane			1.33694E-06		0		1.33694E-	J6 17	
n-Pentane			2 842F-07		0		2 842F-0)7)7	
i-Hexane			0		0		2.0422	0	
Heptane			0		0			0	
Octane			0		0			0	
Nonane			0		0			0	
Benzene			0		0			0	
I oluene	^		0		0			0	
Ethylbenzen m-Xylene	e		0		0			0	
n-Hexane			5.88414E-07		0		5.88414E-	07	
2,2,4-Trimethylpe	ntane		0		0			0	
Neopentane	;		0		0			0	
DecanesPlu	S		0		0			0	
Water			0		0			0	
Helium			0		0			0	
			0		0			0	
	le		0		0 156975		0 15697	75	
Total	10		0.00400282		0.156975		0.16097	78	
Remarks									
			Compon	ent Recove	ries - Projec	t Outlet	S		Status: Solved
			Recovery Stre	am Data So		Itletsin	Project		
Flowsh	eet		PStream	n		owsheet			PStream
Pipeline L	iquids		SalesG	as	Pipe	eline Liquid	ls		TankLiquids
Pipeline L	iquids		TankFla	sh		1-1-0			11.1.1
•	·				• 				
				Parar	neters				
Composition Basi	S		MolarFlow		Summation	Option		Strea	amsand
								Sun	nmation
Calculate Ratios			False		Atomic Basi	S			False

			Recoveri	es Report			
Client Name:	TCEnerg	IY			Job: Pipeli	ne Liquid	sA18-A20
Location:	Ceredo C	compressor Station					
			Tabada				
		Disclined invide Octor	Tabula		Disatis di sui da 7		0
Index		Gas	Fipeline Li Fla	quids:iank ish ol/b	Liquids	anĸ	
Carbon Dioxi	de	IBIII0//II		60283E-06	7 43317	E-06	1 7036E-05
Nitrogen			1	.90265E-05	1.47996	E-06	2.05064E-05
Methane				0.00282028	0.00065	8168	0.00347845
Ethane			0	.000179022	0.00029	9012	0.000469142
Propane				1.9439E-06	1.22781	E-05	1.4222E-05
i-Butane			5	.14445E-08	8.09162	E-07	8.60606E-07
n-Butane			5	.53256E-08	1.28162	E-06	1.33694E-06
i-Pentane			5	.70164E-09	3.86575	E-07	3.92276E-07
n-Pentane	•			3.0496E-09	2.81151	E-07	2.842E-07
I-Hexane				0		0	0
				0		0	0
Nonane			1	<u>0</u>		0	0
Benzene				0		0	0
Toluene				0		0	0
Ethylbenzer	ne			0		0	0
m-Xylene				0		0	0
n-Hexane			2	.47216E-09	5.85942	E-07	5.88414E-07
2,2,4-Trimethylp	entane			0		0	0
Neopentan	е			0		0	0
DecanesPlu	us			0		0	0
Water				0		0	0
Hellum				0		0	0
- Hydrogen				0		0	0
	nle		0	000128082	0 156	847	0 156975
Total	pic		0	00315808	0.150	5782	0.160978
- Otdi				0.00010000	0.10	102	0.100010
Remarks							
	•	Compoi	nent Recove	ries - Projec	ct Losses		Status: Solved
		Reference Str	eam Data So	urce - All O	utlets in Project		
Flowe	heet	PStraz	m		lowsheet		PStream
Pipeline	Liquids	SalesC	ias	Pipe	eline Liquids		TankLiguids
Pipeline	Liquids	TankFla	ash				
•	•						
		Recovery Str	eam Data So	purce - All II	nlets in Project	-	
Flows	heet	PStrea	m	FI	lowsheet		PStream
Pipeline	Liquids	GasSam	nple	Pipe	eline Liquids		LiquidsSample
			Parar	neters			
Composition Bas	sis	Molar Flow		Summation	Option	Summa	ation Only
Calculate Ratios		False		Atomic Bas	is		False
			Tabula	ed Data			
		Summary Table	lavala				
Index		Ihmol/h					
Carbon Dioxi	de	-3.3613F-21					
Nitrogen	-	0	1		1		
Methane		0					
Ethane		-1.07562E-19					
Propane		-5.04195E-21					

Г

Client Name: TC Energy Job: Pipeline Liquids A18-A Location: Ceredo Compressor Station	
Location: Ceredo Compressor Station	-A20
Tabulated Data	
Summary Table	
Index IDMOI/N	
i-Pentane -1.05041E-22	
n-Pentane -5.25203E-23	
i-Hexane 0	
Heptane 0	
Octane 0	
Nonane 0	
Benzene 0	
Toluene 0	
Ethylbenzene 0	
m-Xylene 0	
n-Hexane -2.10081E-22	
Z,Z,4-Inmenylpentane 0	
Under Control	
Hvdrogen 0	
Oxygen 0	
LiquidsSample -2.75358E-17	
Total -2.75358E-17	
Component Recoveries - Project Recoveries	Status: Solved
Reference Stream Data Source - All Inlets in Project	
Flowsheet PStream Flowsheet PS	PStream
Flowsheet PStream Flowsheet PStream Flowsheet P	PStream
Flow sheet PStream Flow sheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui	PStream uidsSample
Flowsheet PStream Flowsheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui	PStream uidsSample
Flowsheet PStream Flowsheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui Recovery Stream Data Source - All Outlets in Project	PStream uidsSample
Flowsheet PStream Flowsheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui Recovery Stream Data Source - All Outlets in Project P Flowsheet PStream Flowsheet P	PStream uidsSample PStream
Flowsheet PStream Flowsheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui Recovery Stream Data Source - All Outlets in Project P Flowsheet PStream Flowsheet P Pipeline Liquids Sales Gas Pipeline Liquids Tank	PStream uidsSample PStream ankLiquids
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTankPipeline LiquidsTank FlashFipeline LiquidsTank	PStream uidsSample PStream ankLiquids
Flow sheet PStream Flow sheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui Recovery Stream Data Source - All Outlets in Project Flow sheet PStream Flow sheet P Pipeline Liquids Sales Gas Pipeline Liquids Tank Flash	PStream uidsSample PStream ankLiquids
Flow sheet PStream Flow sheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui Recovery Stream Data Source - All Outlets in Project Flow sheet PStream Flow sheet P Pipeline Liquids Sales Gas Pipeline Liquids Tan Pipeline Liquids Tank Flash P	PStream uidsSample PStream ankLiquids
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPParametersComposition BasisMolar FlowSummation OptionStreamsan	PStream uids Sample PStream ank Liquids
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPParametersComposition BasisMolar FlowSummation OptionSummationSummationSummation	PStream uids Sample PStream ankLiquids and tion
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPipeline LiquidsTanParametersComposition BasisMolar FlowSummation OptionStreams and SummationCalculate RatiosTrueAtomic BasisFal	PStream uids Sample PStream ankLiquids and tion alse
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPipeline LiquidsTanComposition BasisMolar FlowSummation OptionStreams and SummationCalculate RatiosTrueAtomic BasisFal	PStream uids Sample PStream ankLiquids and tion alse
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPipeline LiquidsTanComposition BasisMolar FlowSummation OptionStreams and SummationCalculate RatiosTrueAtomic BasisFalTabulated Data	PStream uids Sample PStream ankLiquids and tion alse
Flow sheet PStream Flow sheet P Pipeline Liquids Gas Sample Pipeline Liquids Liqui Recovery Stream Data Source - All Outlets in Project Flow sheet PStream Flow sheet P Pipeline Liquids SalesGas Pipeline Liquids Tan Pipeline Liquids SalesGas Pipeline Liquids Tan Pipeline Liquids TankFlash Parameters Summation Option Streamsan Composition Basis Molar Flow Summation Option Streamsan Calculate Ratios True Atomic Basis Fal Tabulated Data Pipeline Liquids:Sales Pipeline Liquids:Tank Pipeline Liquids:Tank Sumation V % % % % %	PStream uids Sample PStream ank Liquids and tion alse Summary Table
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPipeline LiquidsTanComposition BasisMolar FlowSummation OptionStreams ar SummaticCalculate RatiosTrueAtomic BasisFalTabulated DataPipeline Liquids:Sales GasPipeline Liquids:Tank FlashPipeline Liquids:Tank LiquidsSIndex%%%%%	PStream uids Sample PStream ank Liquids and tion alse Summary Table %
FlowsheetPStreamFlowsheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlowsheetPStreamFlowsheetPPipeline LiquidsSalesGasPipeline LiquidsTanPipeline LiquidsTankFlashPipeline LiquidsTanParametersComposition BasisMolar FlowSummation OptionStreams and Summation OptionSt	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTankFlashParametersPComposition BasisMolar FlowSummation OptionStreams an SummationCalculate RatiosTrueAtomic BasisFalTabulated DataPipeline Liquids:Sales Gas %Pipeline Liquids:Tank Flash %Pipeline Liquids:Tank LiquidsPipeline Liquids:Tank Sales %Pipeline Liquids:Tank LiquidsPipeline Liquids:Tank LiquidsSIndex%%%%%SMethane92.78297.2170618.92131	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100 100
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPipeline LiquidsTanOpposition BasisMolar FlowSummation OptionStreams and SummationCalculate RatiosTrueAtomic BasisFallTabulated DataPipeline Liquids:Sales GasPipeline Liquids:Tank FlashPipeline Liquids:Tank LiquidsSIndex%%%92.78297.21706Methane92.78297.21706Methane81.078718.9213Ethane938.159561.840594.0594.05	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100 100 100
FlowsheetPStreamFlowsheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlowsheetPStreamFlowsheetPPipeline LiquidsSalesGasPipeline LiquidsTanPipeline LiquidsSalesGasPipeline LiquidsTanPipeline LiquidsTankFlashPComposition BasisMolar FlowSummation OptionStreams an SummationCalculate RatiosTrueAtomic BasisFalTabulated DataPipeline Liquids:Sales GasPipeline Liquids:Tank FlashPipeline Liquids:Tank LiquidsSIndex%%%%Carbon Dioxide56.367943.6321SNitrogen92.78297.21706MethaneMethane81.078718.9213EthanePropane13.668386.3317	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100 100 100 100
FlowsheetPStreamFlowsheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlowsheetPPipeline LiquidsSalesGasPipeline LiquidsTanPipeline LiquidsSalesGasPipeline LiquidsTanPipeline LiquidsTankFlashParametersComposition BasisMolar FlowSummation OptionStreamsanCalculate RatiosTrueAtomic BasisFalTabulated DataPipeline Liquids:Sales GasPipeline Liquids:Tank FlashPipeline Liquids:Tank LiquidsSIndex%%%Carbon Dioxide56.367943.6321SNitrogen92.78297.21706Methane81.078718.9213Ethane38.159561.840586.33171.940223Propane13.668386.33175.977794.0223	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100 100 100 100 100
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsSales GasPipeline LiquidsTanPipeline LiquidsTank FlashPipeline LiquidsTanParametersComposition BasisMolar FlowSummation OptionStreamsauCalculate RatiosTrueAtomic BasisFalTabulated DataPipeline Liquids:Sales GasPipeline Liquids:Tank ShortPipeline Liquids:Tank LiquidsSIndex%%%%Carbon Dioxide92.78297.21706SMethane81.078718.9213Ethane81.0787Ethane38.159561.8405SPropane13.668386.3317I-Butane5.977794.0223n-Butane4.1382295.8618	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100 100 100 100 100 100
Flow sheetPStreamFlow sheetPPipeline LiquidsGas SamplePipeline LiquidsLiquiRecovery Stream Data Source - All Outlets in ProjectFlow sheetPStreamFlow sheetPPipeline LiquidsSales GasPipeline LiquidsTarPipeline LiquidsSales GasPipeline LiquidsTarPipeline LiquidsTankFlashParametersSummation OptionStreams and SummationComposition BasisMolar FlowSummation OptionStreams and SummationSummationCalculate RatiosTrueAtomic BasisFalPipeline Liquids:Sales GasPipeline Liquids:Tank SummationSummationSIndex%%%%Carbon Dioxide56.367943.6321SNitrogen92.78297.21706Methane81.078718.9213Ethane38.159561.8405Propane13.668386.3317Propane4.1382295.86181.4534898.5465i-Pentane4.1382295.86181.4534898.5465	PStream uids Sample PStream ank Liquids and tion alse Summary Table % 100 100 100 100 100 100 100

* User Specified Values ? Extrapolated or Approximate Values ProMax 5.0.19263.0 Copyright © 2002-2019 BRE Group, Ltd.

			Recoverie	es Report				
Client Name:	TCEnergy	/			Job: Pipeli	ne Liqui	dsA18-A20	
Location:	Ceredo Co	mpressor Station						
			Tabulat	ed Data				
Index		Pipeline Liquids:Sales Gas %	Pipeline Lio Fla %	quids:Tank sh	Pipeline Liquids:T Liquids %	ank	Summary Table	
i-Hexane		70		,	70		70	
Heptane								
Octane								
Nonane								
Benzene								
Toluene								
Ethylbenzen	e							
m-Xylene						700		
n-Hexane				0.42014	99.5	0799	10	00
2,2,4-1 rimethylpe	entane							
Neopentane Decanes Plu	e IS							
Water								
Helium								
Hvdrogen								
Oxygen								
LiquidsSamp	ble			0.081594	99.9	184	1(00
Total				1.96181	98.0	382	1(00
						_		
		Component	Pacovarias	- Pineline I	iquids Inlats		Status Solved	
		Component	Recoveries	- Pipeline L	iquids Inlets		Status: Solved	1
		Component Recovery Strea	Recoveries m Data Sou	- Pipeline L rce - All Inle	iquids Inlets ets in Flowsheet		Status: Solved	1
Flowsh	neet	Component Recovery Strea PStrear	Recoveries m Data Sou n	- Pipeline L rce - All Inle	iquids Inlets ets in Flowsheet		Status: Solved	
Flowsh Pipeline L	neet Liquids	Component Recovery Strea PStream Gas Sam	Recoveries m Data Sou n ⁿ	<mark>- Pipeline L</mark> rce - All Inle Fle Pipe	iquids Inlets ets in Flowsheet owsheet line Liquids		Status Solved PStream Liquids Sample	2
Flowsh Pipeline L	neet Liquids	Component Recovery Strea PStream Gas Sam	Recoveries m Data Sou n ⁿ	<mark>- Pipeline L</mark> rce - All Inle Fle Pipe	iquids Inlets ets in Flowsheet owsheet line Liquids		Status: Solved PStream LiquidsSample	
Flowsh Pipeline L	neet Liquids	Component Recovery Strea PStream Gas Sam	Recoveries m Data Sou n Die Paran	- Pipeline L rce - All Inle Fie Pipe	iquids Inlets ets in Flowsheet owsheet line Liquids		Status: Solved PStream LiquidsSample	
Flowsh Pipeline L Composition Bas	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow	Recoveries m Data Sou n Die Paran	- Pipeline L rce - All Inle Fie Pipe neters Summation	iquids Inlets ets in Flowsheet owsheet eline Liquids Option	St	Status: Solved PStream LiquidsSample	
Flowsh Pipeline L Composition Bas	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow	Recoveries m Data Sou n Die Paran	- Pipeline L rce - All Inle Fle Pipe neters Summation	iquids Inlets ets in Flowsheet owsheet eline Liquids Option	St	Status: Solved PStream Liquids Sample reamsand Summation	
Flowsh Pipeline L Composition Bas Calculate Ratios	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow False	Recoveries m Data Sou n Dle Paran	- Pipeline L rce - All Inle Fle Pipe neters Summation Atomic Basi	<mark>iquids Inlets sets in Flowsheet ow sheet seline Liquids Option s</mark>	Si	Status: Solved PStream Liquids Sample reams and Summation False	
Flowsh Pipeline L Composition Bas Calculate Ratios	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow False	Recoveries m Data Sou ole Paran Tabulat	- Pipeline L rce - All Inle File Pipe Deters Summation Atomic Basi	iquids Inlets ets in Flowsheet ow sheet eline Liquids Option s	Si	Status: Solved PStream Liquids Sample reams and Summation False	
Flow sh Pipeline L Composition Bas Calculate Ratios	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow False Pipeline Liquids:Gas	Recoveries m Data Sou ole Paran Tabulat Pipeline Liau	- Pipeline L rce - All Inle Fle Pipe Deters Summation Atomic Basi ed Data uids:Liquids	iquids Inlets ets in Flowsheet eline Liquids Option s	Si	Status: Solved PStream Liquids Sample reams and Summation False	
Flowsh Pipeline L Composition Bas Calculate Ratios	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow False Pipeline Liquids:Gas Sample	Recoveries m Data Sou n Die Paran Paran Tabulat Pipeline Liqu Sam	- Pipeline L rce - All Inle Fle Pipe neters Summation Atomic Basi ed Data ids:Liquids	iquids Inlets ets in Flowsheet ow sheet eline Liquids Option s Summary Table	St	Status: Solved PStream Liquids Sample treams and Summation False	
Flowsh Pipeline L Composition Bas Calculate Ratios	neet Liquids	Component Recovery Strea PStrear Gas Sam Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h	Recoveries m Data Sou n Die Paran Paran Fipeline Liqu Sam	- Pipeline L rce - All Inle File Pipe neters Summation Atomic Basi ed Data iids:Liquids ple ol/h	iquids Inlets ets in Flowsheet ow sheet eline Liquids Option s Summary Table Ibmol/h	St	Status: Solved PStream Liquids Sample treams and Summation False	
Flow sh Pipeline L Composition Bas Calculate Ratios	neet Liquids	Component Recovery Strea PStrear Gas Sam Gas Sam Holar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05	Recoveries m Data Sou n Die Paran Paran Fipeline Liqu Sam	- Pipeline L rce - All Inle File Pipe neters Summation Atomic Basi ed Data iids:Liquids ple ol/h	iquids Inlets ets in Flowsheet owsheet eline Liquids Option s Summary Table Ibmol/h 1.7036	St S E-05	Status: Solved PStream Liquids Sample reams and Summation False	
Flow sh Pipeline L Composition Bas Calculate Ratios	de	Component Recovery Strea PStrear Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05	Recoveries m Data Sou n Die Paran Paran Fipeline Liqu Sam	- Pipeline L rce - All Inle Fine Pipe Neters Summation Atomic Basi ed Data iids:Liquids ple ol/h 0 0	iquids Inlets ets in Flowsheet owsheet line Liquids Option s Summary Table Ibmol/h 1.7036 2.05064	St St E-05 E-05	Status: Solved PStream Liquids Sample reams and Summation False	
Flow sh Pipeline L Composition Bas Calculate Ratios Calculate Ratios	de	Component Recovery Strea PStrear Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05 0.00347845	Recoveries m Data Sou n Die Paran Paran Fipeline Liqu Sam Ibmo	- Pipeline L rce - All Inle Fin Pipe Neters Summation Atomic Bas ed Data iids:Liquids ple ol/h 0 0	iquids Inlets ets in Flowsheet line Liquids Option s Summary Table Ibmol/h 1.7036 2.05064 0.00347	St St E-05 E-05 7845	Status: Solved PStream Liquids Sample reams and Summation False	
Flow sh Pipeline L Composition Bas Calculate Ratios Calculate Ratios	de	Component Recovery Strea PStrear Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142	Recoveries m Data Sou n Die Paran Tabulat Pipeline Liqu Sam Ibmo	- Pipeline L rce - All Inle Fin Pipe neters Summation Atomic Basi ed Data iids:Liquids ple ol/h 0 0 0	iquids Inlets ets in Flowsheet owsheet line Liquids Option s Summary Table Ibmol/h 1.7036 2.05064 0.00347 d. 4222	51 5 5 5 5 5 5 5 5 5 5 5 5 7 8 45 5 7 8 45 5 7 8 45 5 7 8 45 5 7 8 45 5 7 8 5	Status: Solved PStream Liquids Sample reams and Summation False	
Flow sh Pipeline L Composition Bas Calculate Ratios Calculate Ratios	de	Component Recovery Strea PStrear Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8 60665 0 7	Recoveries m Data Sou n Die Paran Tabulat Pipeline Liqu Sam Ibmo	- Pipeline L rce - All Inle Fin Pipe neters Summation Atomic Basi ed Data iids:Liquids ple ol/h 0 0 0 0	iquids Inlets ets in Flowsheet owsheet line Liquids Option s Summary Table Ibmol/h 1.7036 2.05064 0.00347 0.000463 1.42221	51 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Status: Solved PStream Liquids Sample reams and Summation False	
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Flow sh Pipeline L Composition Bas Calculate Ratios Calculate Ratios Carbon Dioxio Nitrogen Methane Ethane Ethane - Propane i-Butane n-Butane n-Pentane n-Pentane	de	Component Recovery Strea PStrear Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07	Recoveries m Data Sou n Die Paran Tabulat Pipeline Liqu Sam Ibmo	- Pipeline L rce - All Inle Fin Pipe neters Summation Atomic Basi ed Data iids:Liquids ple ol/h 0 0 0 0 0 0 0 0 0 0 0 0	iquids Inlets ets in Flowsheet ow sheet line Liquids Option s Summary Table 1.7036 2.05064 0.00347 0.000463 1.42221 8.60606 1.33694 3.92276 2.842	51 50 50 50 50 50 50 50 50 50 50 50 50 50	Status: Solved	
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Flow sh Pipeline L Composition Bas Calculate Ratios Calculate Ratios Carbon Dioxio Nitrogen Methane Ethane Ethane - Propane - Butane - Butane - Pentane - Pentane - Pentane - Pentane - Pentane - Pentane - Pentane - Pentane - Pentane	de	Component Recovery Strea PStream Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0	Recoveries m Data Sou n Die Paran Tabulat Pipeline Liqu Sam Ibmo	- Pipeline L rce - All Inle Fin Pipe Neters Summation Atomic Bas ed Data iids:Liquids ple ol/h 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	iquids Inlets ets in Flowsheet owsheet line Liquids Option s Summary Table 1.7036 2.05064 0.00347 0.000463 1.42221 8.60606 1.33694 3.92276 2.8421	E-05 E-05 E-05 7845 2142 E-05 E-07 E-06 E-07 E-07 0 0	Status: Solved	
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Flow sh Pipeline L Composition Bas Calculate Ratios Calculate Ratios Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane i-Pentane n-Butane i-Pentane i-Pentane i-Pentane Octane Nonane Benzene Toluene Ethylbenzen	de	Component Recovery Strea Oss Samp Gas Samp Molar Flow False Pipeline Liquids:Gas Sample Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0	Recoveries m Data Sou n Die Paran Tabulat Pipeline Liqu Sam Ibmo	- Pipeline L rce - All Inle Fin Pipe neters Summation Atomic Bas ed Data nids:Liquids ple ol/h 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	iquids Inlets ets in Flowsheet ow sheet line Liquids Option S Summary Table Ibmol/h 1.7036 2.05064 0.00347 0.000463 1.42221 8.60606 1.33694 3.92276 2.8421	E-05 E-05 E-05 7845 2-05 E-07 E-06 E-07 E-07 0 0 0 0 0 0 0 0 0	Status: Solved	
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			Recoverie	es Report			
Client Name:	TCEnergy				Job: Pipelir	neliqu	idsA18-A20
Location:	Ceredo Com	pressor Station					
		·					
			Tabulat	ed Data			
Index	F	Pipeline Liquids:Gas Sample	Pipeline Liqu Sam	uids:Liquids ple	Summary Table	9	
2.2.4-Trimethylpe	entane	n/iomai	mai	01/n	Ibmoi/n	0	
Neopentan	e	0		0		Ő	
DecanesPlu	us	0		0		0	
Water		0		0		0	
Hellum		0		0		0	
Oxygen		0		0		0	
LiquidsSam	ple	0		0.156975	0.156	975	
Total		0.00400282		0.156975	0.160	978	
Bomarka							
Remarks							
							Otatus Oshusil
		Component F	Recoveries -	Pipeline Li	quids Outlets		Status: Solved
		Recovery Stream	n Data Sour	ce - All Outl	lets in Flowsheet		
Flowsh	heet	PStrear	n	Fl	owsheet		PStream
Pipeline I Dipeline	Liquids	SalesGa	as	Pipe	eline Liquids		TankLiquids
Pipeline	Liquids	Тапкта	SI				
			Davar				
Composition Bas	216	MolarElow	Paran	neters	Ontion		treams and
Composition Bas	33	Worarriow		Summation	Option	<u>,</u>	Summation
Calculate Ratios		False		Atomic Basi	S		False
			Tabulat	od Data			
	Р	inalina Liquids Salas		Eu Dala			
		ipenne Liquius.Sales	Pipeline Lie	quids:Tank	Pipeline Liquids:T	ank	Summary Table
Index		Gas	Pipeline Lie Fla	quids:Tank sh	Pipeline Liquids:T Liquids	ank	Summary Table
1 3000010001	da	Gas Ibmol/h	Pipeline Lie Fla Ibm	quids:Tank sh ol/h	Pipeline Liquids:T Liquids Ibmol/h	ank	Summary Table
Nitrogen	de	Gas Ibmol/h	Pipeline Lic Fla Ibm 9	quids:Tank sh ol/h .60283E-06 90265E-05	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1 47998	ank -06	Summary Table Ibmol/h 1.7036E-05 2.05064E-05
Nitrogen	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1	quids:Tank sh ol/h .60283E-06 .90265E-05).00282028	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658	ank E-06 E-06	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845
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Nitrogen Methane Ethane Propane	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 (0.	eu bata quids:Tank sh ol/h .60283E-06 .90265E-05 0.00282028 000179022 1.9439E-06	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781	ank -06 -06 3168 -012 -05	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05
Nitrogen Methane Ethane Propane i-Butane	de	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 (0 0	quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .52256.22	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162	ank -06 -06 3168 -012 -05 -07	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 4.90204E.92
Nitrogen Methane Ethane Propane i-Butane n-Butane	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 0 0 0 0 5 5 5 5 5	quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.227811 8.09162 1.28162 3.86575	ank -06 -06 3168 012 -05 -07 -06 -07	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 1 0 0 0 5 5 5 5 5	quids:Tank sh 60/h 90265E-05 0.00282028 000179022 1.9439E-06 1.14445E-08 .53256E-08 .70164E-09 3.0496E-09	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 3168 012 -05 -07 -06 -07	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane	de	Gas Ibmol/h	Pipeline Lid Fla Ibm 9 1 1 0 0 0 5 5 5 5 5 5 5 5 5	quids:Tank sh ol/h .60283E-06 .90265E-05 .0.00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.865751 2.81151	ank -06 -06 3168 012 -05 -07 -06 -07 -06 -07 -07 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Heptane	de	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 0 0 0 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 -06 -07 -05 -07 -06 -07 -07 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0
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Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Hexane Heptane Octane Nonane	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 (0 0 5 5 5 5 5 5	quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.865751 2.81151	ank -06 -06 -07 -05 -07 -05 -07 -06 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.000347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 (0 0 5 5 5 5 5 5	quids:Tank sh 60/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 -07 -05 -07 -05 -07 -06 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzer	ide	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 (0 0 5 5 5 5 5 5 5 5	eu Data quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 -07 -05 -07 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene	de	Gas Ibmol/h	Pipeline Lie Fla Ibm 9 1 (0 0 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.00025 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 -07 -05 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene n-Hexane	de	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 1 (0 0. 5 5 5 5 5 5 5 5 5 5 5 5 2 5 5 2 5 2 5	quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 3168 012 -05 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene n-Hexane 2,2,4-Trimethylp	ide	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 1 0 0 5 5 5 5 5 5 5 5 5 5 5 2 5 2 5 2 5 2	Europatia quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 .00496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.227811 8.09162 1.28162 3.86575 2.811511	ank -06 -06 3168 012 -05 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene n-Hexane 2,2,4-Trimethylp Neopentan	ide	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 1 0 0 5 5 5 5 5 5 5 5 5 5 5 2 2 2 2	Europatia quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 .0496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 3168 012 -05 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene 2,2,4-Trimethylpp Neopentan DecanesPlu	ide	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 1 (0 0. 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 2 2 2 2	Quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.479961 0.000653 0.00029 1.22781 8.09162 1.28162 3.86575 2.811511 5.859421	ank -06 -06 3168 012 -07 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Nitrogen Methane Ethane Propane i-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene n-Hexane 2,2,4-Trimethylp Neopentan DecanesPlu Water Helium	de	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 1 (0 0. 5 5 5 5 5 5 5 5 5 5 5 5 2 2 2 2	Cu Data quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 .0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.479961 0.000658 0.00029 1.22781 8.09162 1.28162 3.865751 2.811511 5.859421	ank -06 -06 3168 0012 -07 -07 -07 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0
Nitrogen Methane Ethane Propane i-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene n-Hexane 2,2,4-1 rimethylp Neopentan Decanes Plu Water Helium Hydrogen	de	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 0 0 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 2 5 5 2 2 2 2	eu Data quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0 0 0 0 0 0 0 0 0 0 0 0 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 3168 0012 -07 -07 -06 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0
Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzer m-Xylene n-Hexane 2,2,4-1 rimethylp Neopentan Decanes Plu Water Helium Hydrogen Oxygen	ide	Gas Ibmol/h	Pipeline Lio Fla Ibm 9 1 0 0 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	Cu Data quids:Tank sh ol/h .60283E-06 .90265E-05 .00282028 000179022 1.9439E-06 .14445E-08 .53256E-08 .70164E-09 3.0496E-09 0	Pipeline Liquids:T Liquids Ibmol/h 7.43317 1.47996 0.000658 0.00029 1.22781 8.09162 1.28162 3.86575 2.81151	ank -06 -06 3168 0012 -07 -07 -06 -07 -07 0 0 0 0 0 0 0 0 0 0 0 0 0	Summary Table Ibmol/h 1.7036E-05 2.05064E-05 0.00347845 0.000469142 1.4222E-05 8.60606E-07 1.33694E-06 3.92276E-07 2.842E-07 0

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				Recoveri	es Report				
Client Name:	TCEner	gy	mor Station				Job: Pipelin	eLiqu	idsA18-A20
Location:	Celedo	Comple							
				Tabulat	ed Data				
	Í	Pipe	line Liquids:Sales	Pipeline Li	guids:Tank	Pipeli	ne Liquids:Ta	ank	Summary Table
		•	Gas	Fla	sh	•	Liquids		-
Index			lbmol/h	lbm	ol/h		Ibmol/h	700	Ibmol/h
I otal					0.00315808		0.15	782	0.160978
Remarks									
	•		Component	Pocovorios.	Dipolino	iquide L	0650.6		Status: Solved
			Poforonce Street	m Data Sau		Hote in C	lowchoct		
			Reference Strea	m Data Sou	ce - All Out		Towsneet		
Pineline I	iauids		Sales G	n as	FI Pine	eline Liquid	ds		Tankliquids
Pipeline L	iquids		TankFla	sh	1 100				rankEigulas
•	•								
			Recovery Strea	im Data Sou	rce - All Inle	ets in Fl	owsheet		
Flowsh	eet		PStream	n	FI	owsheet			PStream
Pipeline L	iquids		Gas Sam	ple	Pipe	eline Liquio	ds		LiquidsSample
				Parar	neters	0 1			
Composition Basi	S		MolarFlow		Summation	Option		Sumn	nation Only
Calculate Ratios			T alse		Atomic Bas	15			False
				Tabulat	ed Data				
			Summary Table						
Index			lbmol/h						
Carbon Dioxic	le		-3.3613E-21						
Nitrogen			0						
Ethane			-1.07562E-19						
Propane			-5.04195E-21						
i-Butane			-1.05041E-22						
n-Butane			-2.10081E-22						
n-Pentane			-1.03041E-22 -5.25203E-23	}					
i-Hexane			0						
Heptane			0						
Octane			0						
Benzene			0	ł					
Toluene			0						
Ethylbenzen	e		0						
m-Xylene			0						
n-Hexane 2 2 4-Trimethylpe	ntane		-2.10081E-22						
Neopentane			0	1					
DecanesPlu	S		0	<u> </u>					
Water			0						
Helium			0						
Oxygen			0	1					
LiquidsSamp	le		-2.75358E-17	1					
Total			-2.75358E-17						
Remarks									

				Recoveri					
Client Name:	TCEner	gy				Job	: Pipeline Liqui	dsA18-A20	
Location:	Ceredo	Compre	essor Station						
		_							
	•		Component Bo	anvarian D	inalina Ligu	uido Do oovo	rico	Status: So	lved
			Component Re	coveries - P		lius Recove		Olalus. Ol	nveu
			Reference Strea	m Data Sou	rce - All Ini	ets in Flows	sneet		
Flowsh	eet		PStrear	n	FI	owsheet		PStream	
Pipeline L	iquids		Gas Sample Pipeline Liquids				LiquidsSample		
							• · ·		
			Recovery Stream	n Data Sour	ce - All Out	lets in Flow	sheet		
Flowsh	eet		PStream	n	FI	owsheet		PStream	
Pipeline L	iquids		SalesGa	IS	Pipe	eline Liquids		TankLiquids	
Pipeline L	iquias		TankFla	sn					
				Paran	neters				
Composition Basi	S		MolarFlow		Summation	Option	Si	treamsand	
Calculate Ratios							8	False	
Calculate Ratios			The		Atomic Das	5		raise	
				Tabulat	ad Data				
						D:			
		Pipe	line Liquids:Sales	Pipeline Li	quids:Tank	Pipeline Li	quids:Tank	Summary Ta	ble
Index			Gas %	Fia %	sn		ulas 6	%	
Carbon Dioxic	le		70	,	56.3679	,	43.6321	70	100
Nitrogen					92.7829		7.21706		100
Methane					81.0787		18.9213		100
Ethane					38.1595		61.8405		100
Propane					13.6683		86.3317		100
I-Butane					5.9777		94.0223		100
i-Pentane					4.13022		98.5465		100
n-Pentane					1.07305		98.927		100
i-Hexane									
Heptane									
Octane									
Nonane									
Benzene									
Fthylhenzen	e.								
m-Xvlene	5								
n-Hexane					0.42014		99.5799		100
2,2,4-Trimethylpe	ntane								
Neopentane	•								
DecanesPlu	S								
VVater Helium									
Hvdrogen									
Oxvaen									
LiquidsSamp	le				0.081594		99.9184		100
Total					1.96181		98.0382		100
Remarks									

Page 1 of 2

		Er								
Client Name:	TCEner	ду			Jo	ob: Pipeline Liqu	idsA18-A20			
Location:	Ceredo (Compressor Station								
	<u> </u>									
	•	Power	Budget - Pr	niect Power	Budget		Status: Solved			
	<u>.</u>	IOWEI	Buuget - I It	notors	Duuget					
Net Power		0 hr		Total Powe	r Required		0 hp			
Total Power Supp	blied	0 hp)	External En	nergy Only		True			
		·			,					
Remarks	Remarks									
	•	Heat	Budget - Pr	niect Heat B	Rudget		Status: Solved			
		Host Pudget D	ata Source			roject				
		neat Budget D	ata Source		igers in Pr	oject				
Pipeline	iquide	Block DL Liquid T	anks	F	IOW Sheet		Block			
FipelineL	iquius									
			Parar	notors						
Net Duty		-26 2918 Bi	raiai u/h	Total Duty I	Required		0 Btu/b			
Total Duty Suppli	ed	26.2918 Bt	u/h	External En	nergy Only		True			
, , , , , , , , , , , , , , , , , , , ,					,					
			Tabulat	ted Data						
		Block Duty	Block H Tempe	Highest erature	Block Lowe	est Temperature				
Index		Btu/h	0	F To		°F				
Pipeline Liquids:Pl	LIQUID	-18.3342		70		70				
Pipeline Liquids:Se	eparator	-7.95762		71.0182		70				
	<u> </u>									
Remarks										
	·	Power Budo	net - Pipelin	e Liquids Po	ower Budo	net	Status: Solved			
		1 01101 2000	Darar	notors	one budg	J CL				
Net Power		0 hr	raiai	Total Powe	r Required		0 hp			
Total Power Supp	olied	0 hp)	External En	nergy Only		True			
		·								
Remarks										
		Heat Budg	get - Pipelin	e Liquids H	eat Budge	t	Status: Solved			
		Heat Budget Da	ta Source - A	All Exchang	gers in Flo	wsheet				
Flowsh	iquida	Block	onle	F	low sheet		Block			
PipeineL	liquias		an 1KS		enne Liquias		Separator			
Not Duty		00 0040	Parar	Total Duty	Poquired		0 0+/h			
Total Duty Suppli	ed	-26.2918 Bt	u/n u/h	Fytemal En						
	u	20.2310 DI								
			Tabula	ted Data						
		Block Duty	Black	lighost	Block Lewis	st Tomporature				
		DIOCK DULY	Tempe	erature	BIOCK LOWE	sciemperature				
Index		Btu/h	° sente	F		°F				
Pipeline Liquids: Pl	Liquid	-18.3342		70		70				

		En	ergy Budgets Rep	ort			
Client Name:	TCEnergy				Job: Pipelin	eLiquio	dsA18-A20
Location:	Ceredo Compre	essor Station					
			Tabulated Data				
Index		Block Duty	Block Highest Temperature °⊑	Block Lo	westTempeı ∘⊏	rature	
Tanks		Dtu/II					
Pipeline Liquids:Se	parator	-7.95762	71.0182			70	
Remarks							



			Process Str All S Tabulated	reams Report treams by Total Phase			
Client Name:	TCEnergy	1			Job: Waste	water Tank A21	
Location:	Ceredo Compr	essor Station					
Flowsheet:	Wastewater						
			Conn	ections			
			Broothing	Elech	Flaching	Liquido	Looding
			(Wastewater)	Flash	(Wastewater)	Liquius	(Wastewater)
From Block				Wastewater		Wastewater	
				Tank		Tank	
To Block							
							•
			Stream (omposition			
			Broathing	Elash	Flaching	Liquide	Loading
			(Wastewater)	Flash	(Wastewater)	Liquius	(Wastewater)
Mole Fraction			%	%	%	%	%
Carbon Dioxide			0 *			0	0 *
Nitrogen			0 *			0	0 *
Methane			0 *			0	0 *
Ethane			0 *			0	0 *
Propane			0 *			0	0 *
i-Butane			0 *			0	0 *
n-Butane			0 *			0	0 *
I-Pentane			0 ^			0	0 ^
n-Pentane			0 *			0	0 *
Hentane			0 *			0	0 *
Octane			0 *			0	0 *
Nonane			0 *			0	0 *
Benzene			0 *			0	0 *
Toluene			0 *			0	0 *
Ethylbenzene			0 *			0	0 *
m-Xylene			0 *			0	0 *
n-Hexane			0 *			0	0 *
2,2,4-Trimethylpe	ntane		0 *			0	0 *
Neopentane			0 *			0	0 *
DecanesPlus			0 *			0	0 *
Water			100 ^			95	100 ^
Hellum			0 *			0	0 *
			0 *			0	0 *
			3 82531E-09 *			5	3 82531E-09 *
Propylene Glycol			0.020012.00			0	0.0200112.00
			-			-	-
			Breathing (Wastewater)	Flash	Flashing (Wastewater)	Liquids	Loading (Wastewater)
Molar Flow			Ibmol/h	Ibmol/h	Ibmol/h	Ibmol/h	Ibmol/h
Carbon Dioxide			0 7	0	0	0	0 ^
Methano			0 7	U	0	0	U ^
Ethano			0,	0	0	0	0
Propane			0,	0	0	0	0 *
i-Butane			0,3	0	0	0	0 *
n-Butane			, 0 ,	Ŭ Û	0	Ū.	0 *
i-Pentane			0,	0	0	0	0 *
n-Pentane			0 *	0	0	0	0 *
i-Hexane			0 '	0	0	0	0 *
Heptane			0 '	0	0	0	0 *
Octane			0 '	0	0	0	0 *
Nonane			0 '	0	0	0	0 *
Benzene			0 '	0	0	0	0 *
I OIUENE			0 '	0	0	0	0 *
			0 7	0	0	0	U ^
n-Hevana				0	0	0	U "
2 2 4-Trimethylpe	ntane		0	0	0	0	0
Neopentane			0,	0	0	0	0 *
					· · · · · · · · · · · · · · · · · · ·	~	v

Page	2	of	6
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Client Name:	TCEnergy				Job: Waste	water TankA21	
Location:	Ceredo Compre	essor Station					
Flowsheet:	Wastewater						
			1	-	1		1
Molar Flow			Breathing (Wastewater) Ibmol/h	Flash Ibmol/h	Flashing (Wastewater) Ibmol/h	Liquids Ibmol/h	Loading (Wastewater) Ibmol/h
DecanesPlus			0 *	0	0	0	0 *
Water			9.42481E-06 *	0	0	1.70304	7.37807E-05 *
Helium			0 *	0	0	0	0 *
Hydrogen			0 *	0	0	0	0*
			3.60528E-16 *	0	0	0.0896339	2 82234E-15 *
Propylene Glycol			0.000202.10	0	0	0	0 *
			-	-	-	-	-
			Breathing (Wastewater)	Flash	Flashing (Wastewater)	Liquids	Loading (Wastewater)
Mass Fraction			%	%	%	%	%
Carbon Dioxide			0			0	0
NITTOGEN			0			0	0
Fthane			0			0	0
Propane			0			0	0
i-Butane			0			0	0
n-Butane			0			0	0
i-Pentane			0			0	0
n-Pentane			0			0	0
i-Hexane			0			0	0
Heptane			0			0	0
Octane			0			0	0
Nonane			0			0	0
Benzene			0			0	0
Ethylbenzene			0			0	0
m-Xylene			0			0	0
n-Hexane			0			0	0
2,2,4-Trimethylpent	ane		0			0	0
Neopentane			0			0	0
DecanesPlus			0			0	0
Water			100			47.3896	100
Helium			0			0	0
Hydrogen			0			0	0
Oxygen						52 6104	
Propylene Glycol			0.00001E-00			52.0104	0.00001E-00
						U	
Mass Flow			Breathing (Wastewater) Ib/h	Flash Ib/h	Flashing (Wastewater) Ib/h	Liquids Ib/h	Loading (Wastewater) Ib/h
Carbon Dioxide			0 *	0	0	0	0 *
Nitrogen			0 *	0	0	0	0 *
Methane			0 *	0	0	0	0 *
⊨tnane Bropono			0 *	0	0	0	0 *
riopane i-Butane			U ^	0	U	0	U ^
n-Butane			0 * 0 *	0	0	0	0 * 0 *
i-Pentane			0 *	0	0	0	0 *
n-Pentane			0 *	0	Ŭ Ŭ	0	0 *
i-Hexane			0 *	0	Ŭ Ŭ	0	0 *
Heptane			0 *	0	0	0	0 *
Octane			0 *	0	0	0	0 *
Nonane			0 *	0	0	0	0 *
Benzene			0 *	0	0	0	0 *
Toluene			0 *	0	0	0	0 *
Ethylbenzene			0 *	0	0	0	0 *
m-Xylene			0 *	0	0	0	0 *
			U "	U	U	U	Crown Inc. and Affiliates

			Process Str All St Tabulated b	eams Report reams by Total Phase					
Client Name:	TCEnergy				Job: Waste	water Tank A21			
Location:	Ceredo Comp	ressor Station							
Flowsheet:	Wastewater								
Mass Flow			Breathing (Wastewater) Ib/h	Flash Ib/h	Flashing (Wastewater) Ib/h	Liquids Ib/h	Loading (Wastewater) Ib/h		
2,2,4-Trimethylpent	ane		0 *	0	0	0	0 *		
Neopentane			0 *	0	0	0	0 *		
DecanesPlus			0 *	0	0	0	0 *		
Water			0.000169791 *	0	0	30.6808	0.00132918 *		
Helium			0 *	0	0	0	0 *		
Hydrogen			0 *	0	0	0	0 *		
Oxygen			0 *	0	0	0	0 *		
Lube Oil			1.37001E-13 *	0	0	34.0609	1.07249E-12 *		
Propylene Glycol			0 *	0	0	0	0 *		
			Stream	Properties					
Property		Units	Breathing (Wastewater)	Flash	Flashing (Wastewater)	Liquids	Loading (Wastewater)		
Temperature		°F	70.278	60 *	70.278	60	70.278		
Pressure		psia	0.366931	14.6959 *		14.6959	0.366931		
Mole Fraction Vapo	or	%	100		100	0	100		
Mole Fraction Light	Liquid	%	0			5.00236	0		
Mole Fraction Heav	/y Liquid	%	0			94.9976	0		
Molecular Weight		lb/lbmol	18.0153			36.1145	18.0153		
Mass Density		lb/ft^3	0.00116278			58.9286	0.00116278		
Molar Flow		lbmol/h	9.42481E-06	0	0	1.79268	7.37807E-05		
Mass Flow		lb/h	0.000169791	0	0	64.7417	0.00132918		
Vapor Volumetric F	low	ft^3/h	0.146021	0	0	1.09865	1.1431		
Liquid Volumetric F	low	gpm	0.0182052	0	0	0.136974	0.142517		
Std Vapor Volumet	ric Flow	MMSCFD	8.58376E-08	0	0	0.016327	6.71966E-07		
Std Liquid Volumet	ric Flow	sgpm	3.39424E-07	0	0	0.136986	2.65713E-06		
Compressibility			0.999608			0.00161496	0.999608		
Specific Gravity			0.622021			0.944842	0.622021		
API Gravity		B <i>i u</i>				18.2605			
Enthalpy		Btu/n	-0.980386	0	0	-236493	-7.6748		
Mass Enthalpy		Btu/Ib	-5774.09			-3652.87	-5774.09		
Mass Cp	•	Btu/(ID**F)	0.44869			0.695212	0.44869		
Dynamic Viscosity	10	сP	1.32583			62 1742	1.32583		
Kinomotio Viscosity	,		0.00962696			66 0257	0.00962696		
Thermal Conductiv	+. /		0.0116904			00.9257	0.0116904		
Surface Tension	ity		0.0110094			0.190002	0.0110094		
Net Ideal CasHoat	ng Value	Btu/ftA3	6 95865E-07			900 552	6 95865E-07		
Net Liquid Heating	Value	Btu/lb	-1059.76			8979.21	-1059.76		
Gross Ideal Gas He	ating Value	Btu/ft^3	50 31			1013 94	50 31		
Gross Liquid Heatin	ngValue	Btu/lb	1.54535E-05			10076 1	1.54535E-05		
			1.040002-00			10070.1	1.040002-00		
Remarks									
			Process Str All Si Tabulated b	eams Report treams by Total Phase					
---------------------	---------------	---------------	--------------------------------------	---	------------	--------------	--	--	--
Client Name:	TCEnergy				Job: Waste	waterTankA21			
Location:	Ceredo Compre	essor Station							
Flowsheet:	Wastewater								
			Conn	ections	. <u></u>	<u>_</u>			
			Wastewater	Working (Wastewater)					
From Block									
To Block			Wastewater						
			тапк						
Stream Composition									
			Stream	omposition					
Mole Fraction			wastewater %	(Wastewater)					
Carbon Dioxide			0 *	0 *					
Nitrogen			0 *	0 *					
Methane			0 *	0 *					
Ethane			0*	0*					
Propane			0 *	0 *					
n-Butane			0 *	0 *					
i-Pentane			0 *	0 *					
n-Pentane			0 *	0 *					
i-Hexane			0 *	0 *					
Heptane			0 *	0 *					
Nonane			0 *	0 *					
Benzene			0 *	0 *					
Toluene			0 *	0 *					
Ethylbenzene			0 *	0 *					
m-Xylene			0 *	0 *					
n-Hexane	200		0 *	0 *					
Neopentane			0 *	0 *					
DecanesPlus			0 *	0 *					
Water			95 *	100 *					
Helium			0 *	0 *					
Hydrogen			0 ^	0 ^					
			5 *	3 82531E-09 *					
Propylene Glycol			0 *	0 *					
Molor Flow			Wastewater	Working (Wastewater)					
Carbon Dioxide			0 *	0 *					
Nitrogen			0 *	<u> </u>					
Methane			0 *	0 *					
Ethane			0 *	0 *					
Propane			0 *	0 *					
n-Butane			0 *	0 *					
i-Pentane			0 *	0 *					
n-Pentane			0 *	<u> </u>					
i-Hexane			0 *	0 *					
Heptane			0 *	0 *					
Uctane			0 *	0 *					
Renzene			U ^						
Toluene			0 *	0 *					
Ethylbenzene			0 *	0 *					
m-Xylene			0 *	0 *					
n-Hexane			0 *	0 *					
2,2,4-Trimethylpent	ane		0 *	0 *					
Neopentane			0 *	0 *					

		Process Str All S Tabulated I	reams Report treams by Total Phase			
Client Name:	TCEnergy			Job: Waste	waterTankA21	
Location:	Ceredo Compressor Station					
Flowsheet:	Wastewater					
Molar Flow		Wastewater Ibmol/h	Working (Wastewater) Ibmol/h			
DecanesPlus		0 *	0 *			
Water		1.70304 *	3.062E-05 *			
Helium		0 *	0 *			
Hydrogen		0 *	0 *			
Oxygen		0.0806330 *				
Lube Oli		0.0896339	1.17131E-15			
Propylene Glycol		0	0 "			
Mass Fraction		Wastewater %	Working (Wastewater) %			
Carbon Dioxide		,° 0 *	<i>,</i> ,,			
Nitrogen		0 *	0			
Methane		0 *	0			
Ethane		0 *	0			
Propane		0 *	0			
i-Butane		0 *	0			
n-Butane		0 *	0			
i-Pentane		0 *	Ő			
n-Pentane		0 *	0			
i-Hexane		0 *	0			
Heptane		0 *	0			
Octane		0 *	0			
Nonane		0 *	0			
Benzene		0 *	0			
Toluene		0 *	0			
Ethylbenzene		0 *	0			
m-Xylene		0 *	0			
n-Hexane		0 *	0			
2,2,4-Trimethylpent	ane	0 *	0			
Neopentane		0 *	0			
DecanesPlus		0 *	0			
Water		47.3896 *	100			
Helium		0 *	0			
Hydrogen		0 *	0			
Oxygen		0 *	0			
Lube Oil		52.6104 *	8.06881E-08			
Propylene Glycol		0 *	0			
Mass Flow		Wastewater Ib/h	Working (Wastewater) Ib/h			
Carbon Dioxide		0 *	0 *			
Nitrogen		0 *	0 *			
Methane		0 *	0 *			
Ethane		0 *	0 *			
Propane		0 *	0 *			
I-Butane		0 *	0 *			
n-Butane		0 1	0 ^			
n-Pentane		0	0 ^			
n-Pentane		0 *	0 *			
I-Hexane		0 *	U *			
neptane Octano			U ^			
Nonane		0 *				
Ronzono		0 *				
Tolueno			0 *			
Ethylhonzona		U "	U "			
		0 *	U "			
n-Hexano		0 ^	0 ^			
		U "	U "			

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Client Name: TC Energy			Process Streams Report All Streams Tabulated by Total Phase					
Client Name:	TCEnergy					Job: Waster	waterTankA21	
Location:	Ceredo Compr	essor Station						
Flowsheet:	Wastewater							
Mass Flow			Wastewater Ib/h	Working (Wastewater) Ib/h				
2,2,4-Trimethylpent	ane		0 *	0 *	1			
Neopentane			0 *	0 *	<i>.</i>			
DecanesPlus			0 *	· 0 *	·			
Water			30.6808 *	0.000551627 *				
Helium			0 '	0 *	-			
Hydrogen			0 *	0 *	<i>.</i>			
Oxygen			0 *	· 0 *	·			
Lube Oil			34.0609 *	4.45097E-13 *				
Propylene Glycol			0 *	0 *	7			
			Stroom	Proportios				
-			Sueam	Fioperties	-			
Property		Units	Wastewater	Working				
Tana a satura		٥ ٢	CO *	(wastewater)				
		F	60	70.278				
Pressure		psia	14.6959	0.366931				
Mole Fraction Vapo	r Llandal	%	0	100				
Mole Fraction Light		%	5.00236	0				
Molecular Weight	y Liquiu	70 lb/lbmol	94.9970	10.0153				
More Density			30.1143	16.0153				
Maler Flow		ID/II/3	56.9260	0.00116278				
Mora Flow			1.79200	3.062E-05				
Mass Flow	0.17	ID/N	64.7417	0.000551627				
Vapor Volumetric F	0W	10/3/11	1.09865	0.474403				
Liquid Volumetric Fi	OW in Flow	gpm	0.136974	0.0591463				
Std vapor volumet		MINISCED	0.016327	2.76675E-07				
Sta Liquia Volumetr	ICFIOW	sgpm	0.136986 *	1.10274E-06				
Compressibility			0.00161496	0.999608				
A DL Crovity			0.944842	0.622021				
APIGIAVILY		Ptu/b	16.2000	2 1 9 5 1 4				
Enularpy Mass Entheliny		Dlu/II Dtu/Ib	-230493	-3.10314				
Mass Enthalpy			-3052.67	-5774.09				
Mass Cp		Blu/(ID F)	0.095212	0.44609				
Dynamic Viccosity	10	сP	1.10064	1.32363				
Kinomotio Viscosity			66 0257	0.00982898				
Thormal Conductivi	h.,		00.9237	0.0116904				
Surface Tension	ty		0.195502	0.0110094				
Not Ideal Cas Heat			0.0030001	6 058655 07				
Net Liquid Heating	ng value Zaluo	Btu/Ith	909.003 8070 01	0.90000E-07	 			
Gross Ideal Coalles	aiue	Btu/ftA2	1012.04	-1009.70 E0.94				
		Btu/It-3	1013.94	00.31 1 54525E 05				
	y value	Blu/ID	10070.1	1.04030E-00	<u> </u>			
Remarks								

Simulation Initiated on 5/17	Simulation Initiated on 5/17/2021 5:38:14 PM A21_Wastewater_05172021.pmx Page 1						
Energy Stream Report							
Client Name:	TCEnergy	Job: Wastewater TankA21					
Location:	Ceredo Co	do Compressor Station					
Flowsheet:	Wastewate	r					
			Energy Streams				
Energy Stream		Energy Rate	Power	From Block	To Block		
Q-1		0 Btu/h	0 hp		Wastewater Tank		
Remarks							

Simulation Initiated on 5/17	/2021 5:38:14 PM		A21_Wastewate	r_05172021.pmx		Page 1 of 1		
			Blo Wastewa _{Separato}	ncks Iter Tank or Report				
Client Name:	TCEnergy			Job: Wastewater Ta	ankA21			
Location:	Ceredo Compress	or Station			Modified: 3:18 PM,	10/16/2020		
Flowsheet:	Wastewater				Status: Solved 5:36	5 PM, 5/17/2021		
Connections								
Stream	Connection	n Type 💦 🤇	Other Block	Stream	Connection Type	e Other Block		
Wastewater	Inlet			Flash	Vapor Outlet			
Liquids	Light Liquid	Outlet		Q-1	Energy			
			Block Pa	rameters				
Pressure Drop		0	psi	Main Liquid Phase	Li	ght Liquid		
Mole Fraction Va	por	0	%	Heat Duty		0 Btu/h		
Mole Fraction Lig	ht Liquid	5.00236	%	Heat Release Curve T	уре	Plug Flow		
Mole Fraction He	avy Liquid	94.9976	%	Heat Release Curve Increments		10		
Remarks								

		F	owsheet I	Environment PR				
Client Name:	TCEnergy	-			Job: Waste	waterTankA21		
Location:	Ceredo Compi	ressor Station						
Flowsheet:	Wastewater							
Environment Settings								
Number of Poynti	ngIntervals	0		Phase Tolerance		1 %		
Gibbs Excess Mo	del	77 °F		Emulsion Enabled		False		
Evaluation Tempe	erature							
Freeze Out Temp	erature	10 °F						
Threshold Differe	nce							
			Comp	ponents				
Component Name		Henry's Law Component	Phase Initiator	Component Name		Henry's Law Component	Phase Initiator	
Carbon Dioxide		False	False	Toluene		False	False	
Nitrogen		False	False	Ethylbenzene		False	False	
Methane		False	False	m-Xylene		False	False	
Ethane		False	False	n-Hexane		False	False	
Propane		False	False	2,2,4-Trimethylpentane		False	False	
i-Butane		False	False	Neopentane		False	False	
n-Butane		False	False	DecanesPlus		False	False	
I-Pentane		False	False	Vvater		False	Irue	
n-Pentane		False	False	Hellum		Faise	False	
		False	False			False	False	
Octane		False	False			False	False	
Nonane		False	Falsa	Propylene Glycol		False		
Renzene		False	False	Tiopytene Grycol		1 4130	Thức	
Benzene		1 4150	1 0100					
		Dhue		arts Mathad Cata				
Liquid Molor Volum	<u>^</u>	COSTAL	ical Prop	erty wiethod Sets		Bong Bobing	20.0	
Stability Calculation	e	COSTALL Bong Pohing	200	Vapor Package		Peng-Robins		
Light Liquid Packag	0	Peng-Robins	2011	Heavy Liquid Package		Peng-Robins	200	
Eight Eight ackag	0	T chy Robins		Theavy Elquid Tackage		T city Robins		
Remarks								

		Er	nvironm	ents Report			
Client Name:	TCEnergy				Job: Waster	waterTankA21	
Location:	Ceredo Compre	essor Station					
-							
		Р	roject-Wi	de Constants			
Atmospheric Pressu	ire	14.6959	psia	Ideal GasReference Pre	essure	14.6959 p	osia
Ideal Gas Reference	e Temperature	60	°F	Ideal GasReference Vo	lume	379.484 f	t^3/lbmol
Liquid Reference Te	emperature	60	°F				
			Environ	ment[PR]			
		I	Environm	ent Settings			
Number of Poynting Intervals		0		Phase Tolerance		1 %	
Gibbs Excess Mo	del	77 °F		Emulsion Enabled		False	
Evaluation Temperature							
Threeze Out Temperature							
Theatold Dhele							
			0				
			Comp	onents			
Component Name		Henry's Law	Phase	Component Name		Henry's Law	Phase
		C + + + + + + + + +				C	Initiaton
Carbon Dioxide		Component False	Initiator False	Toluene		Component False	Initiator False
Carbon Dioxide Nitrogen		Component False False	Initiator False False	Toluene Ethylbenzene		Component False False	Initiator False False
Carbon Dioxide Nitrogen Methane		Component False False False	Initiator False False False	Toluene Ethylbenzene m-Xylene		Component False False False	Initiator False False False
Carbon Dioxide Nitrogen Methane Ethane		Component False False False False	Initiator False False False False	Toluene Ethylbenzene m-Xylene n-Hexane		Component False False False False	Initiator False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane		Component False False False False False	Initiator False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane		Component False False False False False	Initiator False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane		Component Falæ Falæ Falæ Falæ Falæ Falæ	Initiator False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane		Component False False False False False False	Initiator False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane		Component Falæ Falæ Falæ Falæ Falæ Falæ Falæ	Initiator False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus		Component False False False False False False False False	Initiator False False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane		Component Falæ Falæ Falæ Falæ Falæ Falæ Falæ Falæ	Initiator False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane Decanes Plus Water		Component False False False False False False False False False	Initiator False False False False False False False True
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane		Component Falæ Falæ Falæ Falæ Falæ Falæ Falæ Falæ	Initiator False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium		Component False False False False False False False False False False	Initiator False False False False False False True False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Pentane i-Hexane		Component False False False False False False False False False False False	Initiator False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen		Component False False False False False False False False False False	Initiator False False False False False False True False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Heptane Optage		Component False False False False False False False False False False False False	Initiator False False False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen		Component False False False False False False False False False False False False False	Initiator False False False False False False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane		Component False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Bropylono Glucol		Component False False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene		Component False False False False False False False False False False False False False False False False	Initiator False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol		Component False False False False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False False True
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene		Component False False False False False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol		Component False False False False False False False False False False False False False False False	Initiator False False False False False False True False False False False False False False True
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene		Component False False False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol		Component False False False False False False False False False False False False False False False	Initiator False False False False False False True False False False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene		Component False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol		Component False False False False False False False False False False False False False	Initiator False False False False False False True False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene	e	Component False False False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False False False False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol		Component False False False False False False False False False False False False False False False False	Initiator False False False False False False False False False False False False False False
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Liquid Molar Volum Stability Calculation	e 1 1 1 1 1 1	Component False Fa	Initiator False	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol erty Method Sets Overall Package Vapor Package Heavy Liquid Package		Component False Fa	Initiator False False False False False False False False False False False False True
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Liquid Molar Volum Stability Calculation Light Liquid Packag	e 1 e	Component False Fa	Initiator False False False False False False False False False False False False False False False False False False Son	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol erty Method Sets Overall Package Vapor Package Heavy Liquid Package		Component False Fa	Initiator False False False False False False False False False False False False True
Carbon Dioxide Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Liquid Molar Volum Stability Calculation Light Liquid Packag	e 1 e	Component False Fa	Initiator False False False False False False False False False False False False False False False False False Son	Toluene Ethylbenzene m-Xylene n-Hexane 2,2,4-Trimethylpentane Neopentane DecanesPlus Water Helium Hydrogen Oxygen Lube Oil Propylene Glycol erty Method Sets Overall Package Heavy Liquid Package		Component False Fa	Initiator False False False False False False False False False False False False False True

Client Name:	TCEnergy				Job: Waste	water Tank A21			
Location:	Ceredo Compr	essor Station							
Properties									
Volume Average Point	Boiling	240.832	°F	Low Temperature Vis	cosity	0.441651	cP		
* Molecular Weight		108.848	lb/lbmol	Temperature of High ⁻ Viscosity	Г	210	°F		
 Specific Gravity 		0.7432		High Temperature Vis	cosity	0.256204	cP		
API Gravity		58.8929		Watson K		11.9499			
Critical Temperat	ure	563.715	°F	ASTM D86 10-90% S	lope	0	°F/%		
Critical Pressure		421.397	psia	ASTM D93 Flash Poir	nt	47.9739	°F		
Critical Volume		6.98262	ft^3/lbmol	? Pour Point		-22.4869	°F		
Acentric Factor		0.350921		Paraffinic Fraction		56.3105	%		
Carbon to Hydrog	en Ratio	5.84021		Naphthenic Fraction		29.8859	%		
Refractive Index		1.41346		Aromatic Fraction		13.8037	%		
Temperature of L	owT	100	°F	Ideal GasHeat Capac	ity	38.2665	Btu/(lbmol*°F)		
Viscosity									
Warnings ProMax:ProMax!Pro Warning:	oject!Oils!Decand Pour Point cald	esPlus!Properties!P culation: The value	our Point of 240.832°F	for Volume Average Boiling Po	oint should b	e between 340.33 °	F and 1040.33 °F.		

Remarks

			Single Lu	e Oil Report Ibe Oil			
Client Name:	TCEnergy				Job: Waste	waterTankA21	
Location:	Ceredo Compre	essor Station					
			Pro	operties			
Volume Average Point	Boiling	791.482	°F	Low Temperature Viso	cosity	32.6194	сР
* Molecular Weight		380	lb/lbmol	Temperature of High Viscosity	Γ	210	°F
 Specific Gravity 		0.9		High Temperature Vis	cosity	4.52357	сР
API Gravity		25.7222		Watson K		11.9728	
Critical Temperat	ure	1077.76	°F	ASTM D86 10-90% SI	ope	0	°F/%
Critical Pressure		162.989	psia	ASTM D93 Flash Poir	nt	427.922	°F
Critical Volume		20.2275	ft^3/lbmol	PourPoint		89.7805	°F
Acentric Factor		1.0209		Paraffinic Fraction		58.4435	%
? Carbon to Hydrog	en Ratio	6.55722		Naphthenic Fraction		30.863	%
Refractive Index		1.49164		Aromatic Fraction		10.6935	%
Temperature of Lo Viscosity	owT	100	°F	Ideal GasHeat Capac	ity	133.295	Btu/(lbmol*°F)
Warnings ProMax:ProMax!Pro Warning: 650 °F.	oject!Oils!Lube O Carbon to Hydr	il!Properties!Carbon ogen Ratio calculati	to Hydrogen Ra ion: The value	atio of 791.482 °F for Volume Av	erage Boiling	g Point should be be	tween 80 °F and

Remarks

Client Name:	TOFROM	User Value	Sets Report	Lieb: Worte	unter Text A 24
Client Name:		accor Station		Job: Waste	water LankA21
Location.	Celedo Comple				
				1	
		Proces	e Innute		
* Paramotor			ales Gas Targetj		MMSCED
LowerBound		3 MMSCED	* Enforce Bounds		Falso
Lower Dound			Enleree Beands		1 4155
		Usor Value [W	ator Pato Targot]		
* Parameter					gal/yr
LowerBound			* Enforce Bounds		False
201101 200110					
		User Value [Conc	lonsato Pato Targot]		
* Parameter			Upper Bound		gal/yr
LowerBound		gal/yr	* Enforce Bounds		False
Lower Dound		ganyi	Enlette Beands		1 4156
Remarks					
		Propylene	Glycol Tanks		
* Doromotor					
Falameter			* Enforce Bounds		Falso
Lower Dound			Enfolde Bounds		1 4155
		Llear Value	[Shall angth]		
* Parameter					ft
LowerBound		ft	* Enforce Bounds		False
201101 200110					
		llser Value	[ShollDiam]		
* Parameter		OSET Value	Upper Bound		ft
LowerBound		ft	* Enforce Bounds		False
		llser Value	[Breather//P]		
* Parameter			UpperBound		psig
Lower Bound		psig	* Enforce Bounds		False
		User Value [BreatherVacP1		
* Parameter		-0.03 psig	Upper Bound		psig
Lower Bound		psig	* Enforce Bounds		False
		User Value	[DomeRadius]		
Parameter		ft	Upper Bound		ft
Lower Bound		ft	* Enforce Bounds		False
		User Valu	e [OpPress]		
* Parameter		0 psig	Upper Bound		psig
Lower Bound		psig	* Enforce Bounds		False
		User Value [/	AvgPercentLig]		
* Parameter		50 %	Upper Bound		%
Lower Bound		%	* Enforce Bounds		False
		User Value [MaxPercentLig]		
* Parameter		90 %	Upper Bound		%
Lower Bound		%	 * Enforce Bounds 		False

		User Value	Sets Report			
Client Name:	TCEnergy			Job: Waster	water TankA21	
Location:	Ceredo Compre	essor Station				
		User Value [I	MinPercentLiq]			
* Parameter		10 %	UpperBound			%
LowerBound		%	* Enforce Bounds		False	
		User Value	[AnnNetTP]			
* Parameter		4.69867 bbl/day	Upper Bound			bbl/day
Lower Bound		bbl/day	* Enforce Bounds		False	
		User Val	ue [OREff]			
* Parameter		0 %	Upper Bound			%
LowerBound		%	* Enforce Bounds		False	
		llser Value				
* Parameter		65.4 °F	UpperBound			°F
LowerBound		°F	* Enforce Bounds		False	•
		Llser Value				
* Parameter						°E
LowerBound		*5.5 T	* Enforce Bounds		False	1
Lonor Bound		•	Emoloo Boundo		1 4100	
		Lloor Volu	Dulki aTi			
* Deverseter						
Parameter		58.7899 °F	Upper Bound		Foloo	F
Lower Bound		Γ	Lilloice Boulius		1 alse	
* Demonster		User vai				a da
* Parameter		14.16 psia	Upper Bound		Falco	psia
Lower bound		psia	Enioice Bounds		1 8130	
* Downood for						Disc/fildO/class
^ Parameter		1237 Btu/tt/2/day	Upper Bound		Falsa	Btu/ft^2/day
LowerBound		Btu/It/2/day	Enforce Bounds		False	
		User Value [A	vgWindSpeed]			
* Parameter		4 mi/h	Upper Bound			mi/h
LowerBound		mı/h	* Enforce Bounds		False	
		User Value [MaxH	lourlyLoadingRate]			
Parameter		bbl/hr	Upper Bound		_	bbl/hr
LowerBound		bbl/hr	* Enforce Bounds		False	
		User Value [S	umLiqLevelInc]			
Parameter		ft/yr	UpperBound			ft/yr
LowerBound		ft/yr	* Enforce Bounds		False	
		User Value	[FlashingT]			
* Parameter		70.278 °F	Upper Bound			°F
LowerBound		°F	 * Enforce Bounds 		False	
		User Value [Er	ntrainedOilFrac]			
* Parameter		1 %	Upper Bound			%
LowerBound		%	* Enforce Bounds		False	
		User Value [TurnoverRate1			
* Parameter		68.3814	UpperBound			
LowerBound			* Enforce Bounds		False	

		User Value	e Sets Report		
Client Name:	TC Energy			Job: Waste	waterTankA21
Location:	Ceredo Compre	essor Station			
	· · · ·				
		User Value [LLossSatFactor]		
* Parameter		1.45	Upper Bound		
Lower Bound			* Enforce Bounds		False
		User Value	[AtmPressure]		
* Parameter		14.16 psia	Upper Bound		psia
Lower Bound		psia	* Enforce Bounds		False
		User V	alue [TVP]		
* Parameter		0.258949 psia	Upper Bound		psia
Lower Bound		psia	* Enforce Bounds		False
		User Va	lue [MaxVP]		
* Parameter		0.34849 psia	Upper Bound		psia
Lower Bound		psia	 * Enforce Bounds 		False
		User Va	lue [MinVP]		
* Parameter		0.190248 psia	Upper Bound		psia
Lower Bound		psia	 * Enforce Bounds 		False
		User Value [AvgLiqSurfaceT]		
* Parameter		61.7293 °F	UpperBound		°F
Lower Bound		°F	* Enforce Bounds		False
		User Value [MaxLiqSurfaceT]		
* Parameter		70.278 °F	Upper Bound		°F
Lower Bound		°F	 * Enforce Bounds 		False
		User Value	e [TotalLosses]		
* Parameter		2.54959E-12 ton/yr	Upper Bound		ton/yr
Lower Bound		ton/yr	 Enforce Bounds 		False
		User Value	WorkingLosses]		
* Parameter		1.94953E-12 ton/yr	Upper Bound		ton/yr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value [StandingLosses]		
* Parameter		6.00063E-13 ton/yr	UpperBound		ton/yr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value	RimSealLosses]		
* Parameter		0 ton/yr	UpperBound		ton/yr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value	WithdrawalLoss]		
* Parameter		0 ton/yr	Upper Bound		ton/yr
Lower Bound		ton/yr	^ Enforce Bounds		False
		User Value	LoadingLosses]		
* Parameter		4.6975E-12 ton/yr	Upper Bound		ton/yr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value [Max	HourlyLoadingLoss		
* Parameter		0 lb/hr	Upper Bound		lb/hr

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		User Value	Sets Report		
Client Name:	TC Energy			Job: Waste	waterTankA21
Location:	Ceredo Compre	ssor Station			
			I south at a section of a section		
Lower Bound			HouriyLoadingLoss		Falsa
Lower Bound		ID/III	Enforce Bounds		Faise
			120/1		
Deverseder		User Val	ue [PStar]		
Parameter			• Enforce Bounds		Falso
Lower Bound			Enloice Bounds		T also
* Paramotor					top/ur
LowerBound			* Enforce Bounds		Ealse
Lower Bound		ton/yi	Enleree Beanas		1 4100
* Parameter			Upper Bound		top/yr
LowerBound		ton/vr	* Enforce Bounds		False
					· · · · · · ·
Parameter			UpperBound		lb/hr
LowerBound		Ib/hr	* Enforce Bounds		False
		llser Value [All	CElashinglosses]		
* Parameter			UpperBound		ton/yr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value [Do	ckFittingl osses]		
* Parameter			UpperBound		ton/yr
Lower Bound		ton/vr	* Enforce Bounds		False
		Liser Value (Dr	eckSeaml osses]		
* Parameter			UpperBound		ton/vr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value [F	lashingLosses		
* Parameter			Upper Bound		ton/vr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value [TotalResidual]		
* Parameter		283.565 ton/yr	Upper Bound		ton/yr
Lower Bound		ton/yr	* Enforce Bounds		False
		User Value [C	GasMoleWeight]		
* Parameter		0.0180153 kg/mol	Upper Bound		kg/mol
LowerBound		kg/mol	* Enforce Bounds		False
		User Value [Va	pReportableFrac]		
* Parameter		8.06881E-08 %	Upper Bound		%
LowerBound		%	* Enforce Bounds		False
		User Value [Lic	ReportableFrac]		
* Parameter		52.6104 %	Upper Bound		%
Lower Bound		%	* Enforce Bounds		False
		User Value [Flag	shReportableFrac]		
* Parameter		0 %	Upper Bound		%
Lower Bound		%	 * Enforce Bounds 		False

Client Name:		User Valu	e Sets Report	Lioh: Waste	waterTank 421				
Location:	Ceredo Compre	essor Station		JOD: Waste					
ThisUser Value Set wasprogrammatically generated. GUID={2B36A6D8-C8D1-4CD2-9AE9-43032096E4C0}									
Sum Component Flow/Frac.22									
		User Valu	ie [CompSum]						
* Parameter		0 ton/yr	Upper Bound		ton/yr				
Lower Bound		ton/yr	* Enforce Bounds		False				
Remarks									
ThisUser Value Se	t wasprogramma	atically generated. GUID={4357C5	FC-CEB2-4442-A1F4-459C0	F79940A}					
		Sum Compo	nent Flow/Frac.29						
		User Valu	ue [CompSum]						
* Parameter		6.00063E-13 ton/yr	Upper Bound		ton/yr				
Lower Bound		ton/yr	* Enforce Bounds		False				
		Sum Compo	nent Flow/Frac.30						
* Parameter		User Valu	Lie [CompSum]		top/vr				
LowerBound		ton/yr	* Enforce Bounds		False				
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={9C3A16	55A-84A6-4C39-B59F-E141C	34E0C72}					
		Sum Compo	nent Flow/Frac.31						
		User Valu	ue [CompSum]						
* Parameter		1.94953E-12 ton/yr	Upper Bound		ton/yr				
Lower Bound		ton/yr	Enforce Bounds		Faise				
Remarks ThisUser Value Se	t wasprogramma	atically generated. GUID={071E1B	34-05C2-47CC-A085-38995	27648C5}					
		Sum Compo	nent Flow/Frac.32						
		User Valu	ue [CompSum]						
* Parameter		0 lb/h	Upper Bound		lb/h				
LowerBound		ID/h	" Enforce Bounds		False				
Bomorke									
This User Value Se	t wasprogramma	atically generated. GUID={F5A120	A0-A5E7-452A-A7E7-C242F	A991327}					

		User Value	Sets Report							
Client Name:	TC Energy	amor Station		Job: Waste	waterTankA21					
Location:	Celedo Comple									
				<u> </u>						
		Sum Compone	ent Flow/Frac.33							
			[CompSum]							
* Parameter		1.37001E-13 lb/h	UpperBound		lb/h					
LowerBound		Ib/h	* Enforce Bounds		False					
Remarks ThisUser Value Set wasprogrammatically generated. GUID={CB3705AB-1F89-4C62-BF55-8508907E81B4}										
		Sum Compone	ont Flow/Frac 34							
		Sull compone	FIL FIOW/FIAC.34							
* Paramotor					lb/b					
LowerBound		Ib/h	* Enforce Bounds		False					
Lower Board		10/11	Emoto Boundo		1 0100					
Remarks ThisUser Value Set	t wasprogramma	atically generated. GUID={DCFE8712	2-5BB2-48D4-BC97-394C4	135488B4}						
			/							
		Sum Compone	ent Flow/Frac.35							
		User Value	[CompSum]							
* Parameter		4.45097E-13 lb/h	Upper Bound		lb/h					
Lower Bound		lb/h	* Enforce Bounds		False					
Remarks ThisUser Value Set	t wasprogramma	atically generated. GUID={A5869694	-840B-429A-B69A-1E3888	ACE8B3}						
		Sum Compone	ent Flow/Frac 36							
* Parameter					ton/vr					
LowerBound		ton/vr	* Enforce Bounds		False					
		, ,								
Remarks ThisUser Value Set	t wasprogramma	atically generated. GUID={F59DBD01	E-0AC2-4422-AB61-597DE	381EEC86}						
		Sum Compone	ent Flow/Frac.37							
		User Value	[CompSum]							
* Parameter		0 ton/yr	Upper Bound		ton/yr					
Lower Bound		ton/yr	* Enforce Bounds		False					
Remarks ThisUser Value Set	Remarks ThisUser Value Set wasprogrammatically generated. GUID={21936257-C6B2-46EC-958E-B899560405D5}									
		0								
		Sum Compone	ent Flow/Frac.38							
		User Value	[CompSum]							
Parameter		U ton/yr	opper Bound		ton/yr False					
Remarks										

	1705									
Client Name:	TC Energy	e eest Station		Job: Waste	waterTankA21					
Location:	Celedo Compi									
ThisUser Value Set wasprogrammatically generated. GUID={673602E1-F687-4A48-B880-B62DA6D53544}										
		Sum Compo	onent Flow/Frac.39							
		User Val	ue [CompSum]							
* Parameter		0 ton/yr	UpperBound		ton/yr					
LowerBound		ton/yr	* Enforce Bounds		False					
Remarks ThisUser Value Se	et wasprogramm:	atically generated. GUID={A6687	4FE-5757-4A82-A90D-461551	A14FE0}						
		Sun compo								
* Parameter					lb/b					
LowerBound		lb/h	* Enforce Bounds		False					
		Sum Comp	opent Flow/Frac 41	_						
		Liser Val								
* Parameter		0 lb/h	UpperBound		lb/h					
LowerBound		lb/h	* Enforce Bounds		False					
Remarks ThisUser Value Se	et wasprogramm	atically generated. GUID={15B55	6F6-F294-4267-BD11-BC8C5	F036006}						
		Sum Compo	onent Flow/Frac.42							
		User Val	ue [CompSum]							
* Parameter		0 lb/h	Upper Bound		lb/h					
Lower Bound		lb/h	* Enforce Bounds		False					
Remarks ThisUser Value Se	et wasprogramm	atically generated. GUID={160EB	D9C-29DD-4770-9C07-6B583	A1CF55A}						
		Sum Compo	opent Flow/Frac.43							
		liser Val	ue [CompSum]							
* Parameter		0 lb/h	Upper Bound		lb/h					
LowerBound		Ib/h	* Enforce Bounds		False					
Remarks ThisUser Value Se	et wasprogramm	atically generated. GUID={C0316	A6A-5A27-4BFC-8CB0-59283	A21D199}						

Page 1 of 7

				Recoveri	es Report	:		lob: Wastewater Tank A21			
Client Name:	TCEner	gy Compose	and Station				Job: Waste	waterTankA21			
Location:	Ceredo	Compre	ssor Station								
	<u>.</u>						.				
	•		Compo	nent Deeev		at Inlate			Statue	Solved	
			Compo	nent Recove	eries - Proje	ect miets			Status.	Solved	
			Recovery Stre	eam Data So	purce - All I	nlets in I	Project				
Flowsh	neet		PStrear	n	F	lowsheet		P	Stream		
Wastew	ater		Wastewa	ter							
				Parar	neters						
Composition Basi	S		Molar Flow		Summation	Option		Streamsa	nd		
								Summat	ion		
Calculate Ratios False					Atomic Bas	is		Fa	lse		
				Tabulat	ed Data						
		Wast	ewater:Wastewater	Summa	rv Table						
Index			lbmol/h	lbm	ol/h						
Carbon Dioxi	de		0		0						
Nitrogen			0		0						
Methane			0		0						
Ethane			0		0						
Propane			0		0						
i-Butane			0		0						
n-Butane			0		0						
i-Pentane			0		0						
n-Pentane			0		0						
I-nexalle Hentane			0		0						
Octane			0		0						
Nonane			0		0						
Benzene			0		0						
Toluene			0		0						
Ethylbenzen	е		0		0						
m-Xylene			0		0						
n-Hexane			0		0						
2,2,4-Trimethylpe	entane		0		0						
Neopentane	Э		0		0						
DecanesPlu	IS		1 70204		1 70204						
			1.70304		1.70304						
Hydrogen			0		0					<u> </u>	
Oxvden			0		0						
Lube Oil			0.0896339		0.0896339						
Propylene Gly	/col		0		0						
Total			1.79268		1.79268						
Remarks											
	•										
			Compon	ent Recove	ries - Proje	ct Outlet	S		Status:	Solved	
			Recovery Stre	am Data So	urce - All O	utletsin	Project				
Flowsh	neet		PStream	n	F	lowsheet		P	Stream		
Wastew	ater		Flash	••	I I I I I I I I I I I I I I I I I I I	astewater		F	iquids		
									-1		
				Dorer	notors						
Composition Des			MolerFlow	Farar	Summeter	Ontion		Ctro om = =	nd		
Composition Bas	10		WOIAI FIOW		Summation			Summati	ion		
Calculate Ratios			False		Atomic Bas	is		Fa	lse		
calourato natios			1 4100		,onno Bae			14			

Recoveries Report											
Client Name:	TCEnergy				Job: Wastev	vaterTa	nkA21				
Location:	Ceredo Compr	essor Station									
			Tabulat	ad Data							
	N N	lastewater:Flash	Wastewate	or liquids	Summary Table						
Index		lbmol/h	Ibmo	ol/h	Ibmol/h						
Carbon Dioxid	de			0		0					
Nitrogen				0		0					
Methane				0		0					
Propane				0		0					
i-Butane				0		0					
n-Butane				0		0					
i-Pentane				0		0					
n-Pentane				0		0					
I-Hexane Hontono				0		0					
Octane				0		0					
Nonane				0		õ					
Benzene				0		0					
Toluene				0		0					
Ethylbenzen	e			0		0					
m-Xylene				0		0					
2 2 4-Trimethylpe	Intane			0		0					
Neopentane				0		0					
DecanesPlu	S			0		0					
Water				1.70304	1.70	304					
Helium				0		0					
Hydrogen				0		0					
Lube Oil				0.0896339	0.0896	339					
Propylene Gly	col			0	0.0000	0					
Total				1.79268	1.79	268					
Remarks	Remarks										
								_			
		Compon	ent Recover	ies - Proiec	tLosses		Status: Solve	ed			
	-	Compone Reference Street	ent Recover	ies - Projec	t Losses		Status: Solve	ed			
Elowsh	eet	Compone Reference Stream	ent Recover am Data Sou	<mark>ies - Projec</mark> Irce - All Ou	t Losses utlets in Project		Status: Solve	d			
Flowsh Wastew:	eet ater	Compone Reference Stream PStream Flash	<mark>ent Recover</mark> am Data Sou	<mark>ies - Projec</mark> urce - All Ou Fli Wz	t Losses utlets in Project ow sheet astewater		Status: Solve PStream	ed			
Flow sh Wastewa	eet ater	Compone Reference Stream PStream Flash	ent Recover am Data Sou	<mark>ies - Projec</mark> urce - All Ou Fli Wa	t Losses utlets in Project ow sheet astewater	_	Status: Solve PStream Liquids	ed			
Flow sh Wastewa	eet ater	Compon Reference Stream PStream Flash	ent Recover am Data Sou n pam Data So	<mark>ies - Projec</mark> urce - All Ou Wa	t Losses utlets in Project ow sheet astewater		Status: Solve PStream Liquids	ed			
Flowsh Wastewa	eet ater	Compone Reference Stream PStream Flash Recovery Stream	ent Recover am Data Sou am Data So	<mark>ies - Projec</mark> <mark>Irce - All Ou</mark> Flo Wa urce - All Ir	t Losses utlets in Project ow sheet astewater		Status: Solve PStream Liquids	ed			
Flow sh Wastewa Flow sh Wastewa Flow sh	eet ater eet ater	Compone Reference Strea PStream Flash Recovery Stream Wastewat	ent Recover am Data Sou n eam Data So n er	<mark>ies - Projec</mark> <mark>Irce - All Ot</mark> Flu Wa urce - All Ir Flu	t Losses utlets in Project ow sheet astewater Ilets in Project ow sheet		Status: Solve PStream Liquids PStream	ed			
Flowsh Wastewa Flowsh Wastewa	eet ater eet ater	Compone Reference Strea PStream Flash Recovery Stream Wastewat	ent Recover am Data Sou n eam Data So n er	<mark>ies - Projec</mark> Irce - All Ou Flu Wa urce - All Ir Flu	t Losses utlets in Project ow sheet astewater lets in Project ow sheet		Status: Solve PStream Liquids PStream	ed			
Flow sh Wastewa Flow sh Wastewa	eet ater eet ater	Compone Reference Strea PStrean Flash Recovery Strean Wastewat	ent Recover am Data Sou am Data Sou er Param	ies - Projec irce - All Ou Fla Wa urce - All Ir Fla peters	t Losses utlets in Project ow sheet astewater lets in Project ow sheet		Status: Solve PStream Liquids PStream	ed			
Flow sh Wastewa Flow sh Wastewa Composition Basi	eet ater eet ater S	Compone Reference Strea PStrean Flash Recovery Strea PStream Wastewate Molar Flow	ent Recover am Data Sou am Data Sou am Data So an er Param	ies - Projec Irce - All Ou Fla Wa urce - All Ir Fla Deters Summation	t Losses utlets in Project ow sheet astewater lets in Project ow sheet	Summa	Status: Solve PStream Liquids PStream	ed			
Flow sh Wastew Flow sh Wastew Composition Basi Calculate Ratios	eet ater eet ater S	Compone Reference Strea PStrean Flash Recovery Strea PStream Wastewate Molar Flow False	ent Recover am Data Sou am Data Sou er Param	ies - Project arce - All Ou File Wa urce - All Ir File beters Summation Atomic Bas	t Losses utlets in Project ow sheet astewater lets in Project ow sheet Option s	Summa	Status: Solve PStream Liquids PStream	ed			
Flow sh Wastewa Flow sh Wastewa Composition Basi Calculate Ratios	eet ater eet ater S	Compone Reference Stream Flash Recovery Stream Wastewate Molar Flow False	ent Recover am Data Sou n eam Data Soo er Param	ies - Project arce - All Ou Fli Wa urce - All Ir Fli urce - All Ir Fli Deters Summation Atomic Basi	t Losses utlets in Project ow sheet astewater lets in Project ow sheet Option s	Summa	Status: Solve PStream Liquids PStream tion Only False	ed			
Flow sh Wastewa Flow sh Wastewa Composition Basi Calculate Ratios	eet ater eet ater S	Compon Reference Strea PStrean Flash Recovery Stree PStrean Wastewat Molar Flow False	ent Recover am Data Sou am Data Sou er Paran Paran	ies - Project arce - All Ou Fli Wa urce - All Ir Fli urce - All Ir Fli beters Summation Atomic Basi	t Losses utlets in Project ow sheet astewater lets in Project ow sheet Option s	Summa	Status: Solve PStream Liquids PStream tion Only False	ed			
Flow sh Wastewa Flow sh Wastewa Composition Basi Calculate Ratios	eet ater eet ater S	Compon Reference Strean Flash Recovery Stree PStrean Wastewate Molar Flow False Summary Table	ent Recover am Data Sou am Data Sou er Param Tabulate	ies - Project arce - All Ou Fli Wa urce - All Ir Fli urce - All Ir Fli beters Summation Atomic Basi	t Losses utlets in Project ow sheet astewater hets in Project ow sheet Option s	Summa	Status: Solve PStream Liquids PStream tion Only False	ed			
Flow sh Wastewa Flow sh Wastewa Composition Basi Calculate Ratios	eet ater eet ater S	Compon Reference Strea PStrean Flash Recovery Stre PStrean Wastewat Molar Flow False Summary Table Ibmol/h	ent Recover am Data Sou n eam Data Soo er Param Tabulate	ies - Projec arce - All Ou Fli Wa urce - All Ir Fli Neters Summation Atomic Basi ed Data	t Losses utlets in Project ow sheet astewater lets in Project ow sheet Option S	Summa	Status: Solve	ed			
Flow sh Wastewa Flow sh Wastewa Composition Basi Calculate Ratios	eet ater eet ater S	Compon Reference Strea PStrean Flash Recovery Stre PStrean Wastewat Molar Flow False Summary Table Ibmol/h	ent Recover am Data Sou n eam Data Soo e Param Tabulate	ies - Projec arce - All Ou Flu Wa urce - All Ir Flu Deters Summation Atomic Bas ed Data	t Losses utlets in Project ow sheet astewater lets in Project ow sheet Option s	Summa	Status Solve	ed			
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			Recoveries Report						
Client Name:	TCEnergy				Job: Wastew	ater TankA21			
Location:	Ceredo Co	mpressor Station							
			Tabula	ted Data					
	l.	Summary Table							
n-Butane		Ibmol/h							
i-Pentane		0							
n-Pentane		0							
i-Hexane		0							
Octane		0							
Nonane		0							
Benzene		0							
Toluene		0							
Ethylbenzen m-Xylene	ie	0							
n-Hexane		0							
2,2,4-Trimethylpe	entane	0							
Neopentan	e	0							
DecanesPlu	JS	0							
Helium		0							
Hydrogen		0							
Öxygen		0							
Lube Oil		0							
Propylene Gly	COI	0							
Remarks									
Remarks									
Remarks	_	Compone	ent Recoveri	es - Project	Recoveries	Status: Solved			
Remarks		Compone Reference St	ent Recoverio	es - Project	Recoveries	Status: Solved			
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Remarks	heet vater	Compone Reference St PStre Wastew	ent Recoveri tream Data S am ater	<mark>es - Project ource - All I</mark>	Recoveries nlets in Project owsheet	Status: Solved PStream			
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Client Name: TC Energy Job: Wastewater Tank A21										
Location: Ceredo Compressor Station										
Tabulated Data										
Wastewater:Flash Wastewater:Liquids Summary Table										
Index % % %										
Nonane										
Benzene										
Toluene										
Ethylbenzene										
m-Xylene										
Neopentane										
DecanesPlus										
Water 100 100										
Helium										
Hydrogen										
Propylene Glycol										
Total 100 100										
Remarks										
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Remarks Component Recoveries - Wastewater Inlets Status: Solv	ed									
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Client Name: TC Energy Job: Wastewater Tank A21								
Client Name:	TCEnergy			Job: Wastewa	aterTankA21			
Location:	Ceredo Com	pressor Station						
			Tabulated Data					
	Wa	astewater:Wastewater	Summary Table					
Index		lbmol/h	lbmol/h					
Water		1.70304	1.70304					
Helium		0	0					
Hydrogen		0	0					
Oxygen		0	0					
Lube Oil		0.0896339	0.0896339					
Propylene Gly	col	0	0					
Total		1.79268	1.79268					
Remarks	_	Commona			Status Salvad			
		Componen	t Recoveries - Wastewa	ater Outlets	Status. Solved			
		Recovery Stream	n Data Source - All Out	ets in Flowsheet				
Flowsh	leet	PStream	n Fl	owsheet	PStream			
Wastewa	ater	Flash	W	astewater	Liquids			
			Parameters					
Composition Basi	s	Molar Flow	Summation	Option	Streamsand			
					Summation			
Calculate Ratios		False	Atomic Basi	S	False			
			Tabulated Data					
		Wastewater:Flash	Tabulated Data Wastewater:Liquids	Summary Table				
Index		Wastewater:Flash Ibmol/h	Tabulated Data Wastewater:Liquids Ibmol/h	Summary Table Ibmol/h				
Index Carbon Dioxid	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastewater:Liquids Ibmol/h	Summary Table Ibmol/h	0			
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Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane i-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0			
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Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane i-Pentane i-Pentane n-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane i-Pentane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene 2,2,4-Trimethylpe Decanes Plu	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0 <t< td=""></t<>			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0 1.70304	Summary Table Ibmol/h	0 0			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium Hydrogen	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane n-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium Hydrogen Oxygen	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium Hydrogen Oxygen Lube Oil	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0 <t< td=""></t<>			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium Hydrogen Oxygen Lube Oil Propylene Gly	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0 <t< td=""></t<>			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane i-Pentane i-Hexane Heptane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium Hydrogen Oxygen Lube Oil Propylene Gly	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0 <t< td=""></t<>			
Index Carbon Dioxio Nitrogen Methane Ethane Propane i-Butane n-Butane i-Pentane n-Pentane i-Hexane i-Hexane Octane Nonane Benzene Toluene Ethylbenzen m-Xylene n-Hexane 2,2,4-Trimethylpe Neopentane Decanes Plu Water Helium Hydrogen Oxygen Lube Oil Propylene Gly	de	Wastewater:Flash Ibmol/h	Tabulated Data Wastew ater:Liquids Ibmol/h 0	Summary Table Ibmol/h	0 0 <t< td=""></t<>			

			Recoveries Report								
Client Name:	TCEner	ду						Job: Waste	water T	ankA21	
Location:	Ceredo (Compre	essor Station								
								<u> </u>			
			Compon	on	t Pacovaria	s - Wastow	atorlos	200		Status:	Solved
1	· ·			CI							
			Reference Stre	ear	m Data Sour	ce - All Ou	tiets in F	lowsneet	-		
Flowsh	eet		PStre	ean	n	FI	low sheet			PStream	
wastewa	aler		Fla	Sn		V	astewater			Liquids	
			D = = = = = 0 (m				-1-1-5				
			Recovery Str	ea	m Data Sou	rce - All Ini	ets in Fi	owsneet	-		
Flowsh	eet		PStre	ean	n	FI	lowsheet			PStream	
Wastewa	ater		Waste	wat	ter						
					_						
					Paran	neters					
Composition Basis	S		Molar Flow			Summation	Option		Sumn	nation Only	
Calculate Ratios			False			Atomic Bas	15			False	
					Tabulat	ed Data	•				
		S	Summary Table								
Index			lbmol/h								
Carbon Dioxid	le		0								
Methane			0								
Ethane			0								
Propane			0								
i-Butane			0								
n-Butane			0								
i-Pentane			0								
n-Pentane			0								
I-Hexane Hentane			0								
Octane			0								
Nonane			0								
Benzene			0								
Toluene			0	1							
Ethylbenzene	e		0								
m-Xylene			0								
n-Hexane	ntono		0								
2,2,4-1 Inneuryipe	niane		0								
DecanesPlus	s		0								
Water			0								
Helium			0								
Hydrogen			0								
Oxygen			0								
Lube OII Pronylene Clyr			0								
Total	501		0								
			0		1					1	
Remarks											
Keinarko											
			Componer	nt F	Recoveries -	Wastewate	er Reco	veries		Status:	Solved
			Reference Str	62	m Data Sou	rce - All Inl	ets in Fl	owsheet			
Flowsh	eet		DQtr	20	n	E	lowsheet			PStream	
Wastewa	ater		Waster	wat	ter		ion oneot			i ou cam	
11460110			11000								

			Recoveri								
Client Name:	TCEnergy	/				Job: Wastewate	rTankA21				
Location:	Ceredo Co	ompressor Station									
		•									
<u> </u>											
		Be any any Stream	n Data Sour		lata in El	owohaat					
		Recovery Stream	Il Dala Sour	ince - All Oullets In Flowsheet							
Flowsh	eet	PStrear	n	FI	owsheet		PSt	ream			
Wastewa	ater	Flash		W	astewater		Liq	luids			
	Parameters										
Composition Basis	s	MolarElow	i uiui	Summation	Option		Streamsand	1			
Composition Basis	0	Wordthiow		Cummation	Option		Summation	۰ ۱			
Calculate Ratios	True		Atomic Basi	c		False					
Carculate Matios		The		Atomic Das	3		1 8130	,			
			labulat	ed Data							
		Wastewater:Flash	Wastewate	er:Liquids	Sur	nmary Table					
Index		%	%	0		%					
Carbon Dioxid	le										
Nitrogen											
Methane											
Ethane											
Propane											
i-Butane											
n-Butane											
i-Pentane											
n-Pentane											
i-Hexane											
Heptane											
Octane											
Nonane											
Benzene											
Toluene											
Ethylbenzene	e										
m-Xylene											
n-Hexane											
2,2,4-Trimethylpe	ntane										
Neopentane											
DecanesPlus	S										
Water				100		100					
Helium											
Hydrogen											
Oxygen											
Lube Oil				100		100					
Propylene Glyc	col										
Total				100		100					
Remarks											

	Energy Budgets Report								
Client Name:	TCEnergy	•				Job: Wastewa	terTankA	21	
Location:	Ceredo Compr	essor Station							
	· ·								
		Power	Budget - Pro	oject Powei	r Budget			Status:	Solved
			Parar	neters					
Net Power		0 hp		Total Powe	r Required			0 hp	
Total Power Supp	blied	0 hp)	External Er	nergy Only			True	
Remarks									
		Heat	Rudget - Pro	niect Heat F	Rudaet			Status:	Solved
		Heat Budget D			a age	Droject			
		Heat Budget D	ata Source	- All Exchai	ngersin	Project			
Flowsh	leet	Block	-	F	lowsheet			Block	
Wastew	ater	Wastewater	Lank						
			Parar	neters					
Net Duty		0 Bt	u/h	Total Duty	Required			0 Btu	/h
Total Duty Suppli	ed	0 Bt	u/h	External Er	nergy Only			True	
			Tabulat	ed Data					
		Block Duty	Block H Tempe	lighest erature	Block Lo	west Tempera	ture		
Index		Btu/h	0	F		°F			
Wastewater:Waste	ewater	0		60		6	50		
Tank					<u> </u>				
Remarks					_				
		Power Bu	dget - Wast	ewater Pow	ver Budg	et		Status:	Solved
			Parar	neters					
Net Power		0 hp)	Total Powe	r Required			0 hp	
Total Power Supp	lied	0 hp		External Er	nergy Only			True	
Remarks									
	<u> </u>	Lleat Du	denat Wast	oweter Lles	+ Dudge	4		Status	Solved
		neat Bu	uget - wast	ewater Hea	it budget			Status.	Conved
		Heat Budget Dat	a Source - A	All Exchang	gers in F	lowsheet			
Flowsh	leet	Block		F	lowsheet			Block	
Wastew	ater	Wastewater	Tank						
			Parar	neters					
Net Duty		0 Bt	u/h	Total Duty	Required			0 Btu	/h
Total Duty Suppli	ed	0 Bt	u/h	External Ér	nergy Only			True	
			Tabulat	ed Data					
	1	Pleak Duty	Disal	lighost	Bleek	woot Tomas	ture		
		BIOCK Duty	Block F	ngnest	BIOCK LO	west lempera	ture		
Index		Btu/b	rempe	F		°F			
Wastewater Waste	ewater			60		6	50		
Tank		v		00		C C			
L							1		

		Energy Budgets Report			
Client Name:	TCEnergy		Job: Waste	:WastewaterTankA21	
Location:	Ceredo Compressor Station				
Remarks					