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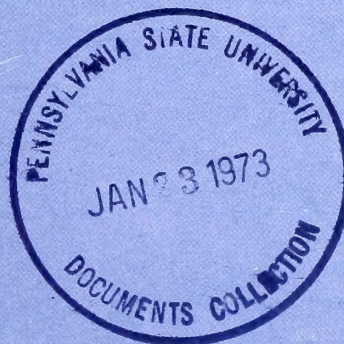
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U.S. DEPARTMENT OF COMMERCE
National Oceanic and Atmospheric Administration
National Marine Fisheries Service



Engineering Economic Model for Fish Protein Concentration Processes

K.K. ALMENAS, L.C. DURILLA, R.C. ERNST,
J.W. GENTRY, M.B. HALE, and J.M. MARCHELLO



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Engineering Economic Model For Fish Protein Concentration Processes

By

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I. ABSTRACT

A process engineering economic model for fish protein concentration processes has been developed. The model predicts the construction and operating costs for fish meal plants and for plants producing fish protein concentrate (FPC) by: isopropyl alcohol extraction, biological, and press cake-isopropyl alcohol extraction.

Typical process flow sheets and a computer program were developed to be used in the design and cost computations. The model provides for each process to be studied both internally and externally in comparison with alternate processes. The program and model were prepared in such a way that changes and updating may be accomplished quite readily as new information becomes available. This report contains directions for users and descriptions of the processes. A listing of the computer program and example calculations for each process are presented in the Appendix to guide the user and to illustrate the nature of the model output.

While the model does develop construction, operating, and production aspects of the processes, it does not deal with the economics of selling the products and the resulting profit and return on investment. Problems of allocation of costs and marketing arrangements are not covered in this report, but must be considered in the final decisions relating to a complete evaluation of alternatives.

II. INTRODUCTION

Fish protein concentrate (FPC) production holds substantial promise of helping to meet the growing food and dietary requirements for the world's human population. It appears that several of the processes now being developed will be successful in making FPC available on a competitive basis with other sources of protein (1, 2). To provide for the orderly and rapid development of these processes it is necessary to continually review the internal steps of each process and to compare processes on a common basis.

The objective of this study was to develop a process cost and design model which can predict construction and operating costs for a wide range of FPC process conditions. The model was to handle a number of the FPC processes, operated singly or in conjunction with associated operations such as fish meal manufacture. This approach of making predesign computer estimates (3, 4) is becoming a common tool of management in process industry research and development.

A. Engineering Economic Model

The model consists primarily of a digital computer program which determines the size and cost of major items of equipment for each process and then estimates the costs. The model is constructed so that new information

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at the bench scale, pilot plant, and demonstration plant levels can be easily incorporated to keep the program current with the available knowledge about each process.

Typical process flow sheets were developed with suitable options for each of the processes. These were used along with the available information on the process to prepare the material and energy balance portions of the program. Changes in flow sheets, types of equipment, processing sequences, and operating conditions, may be made following the internal program changes procedures.

From the material and energy calculations, the major items of equipment are sized and their cost estimated through built-in design and cost information. The program then determines the operating and manufacturing costs subject to the input data and internal assumptions of the model.

Two important features of the program are the built-in consistency of estimates for different processes and the continuity of estimates during the several stages of development of a given process. The uniformity of estimates results primarily from the use of a common set of equipment cost subroutines and a common set of assumptions regarding such cost items as indirect costs, land, engineering, etc. Since input data include the cost of labor, plant size, and cost indices, the program is useful in many broad-based studies of FPC production in different parts of the world at the present and in the future.

The model provides for each FPC process to be studied both internally and externally in comparison with alternate processes. Internal costs identify areas needing further research and development. The ability to estimate costs for a number of processes for a wide range of input conditions provides the broad comparison type information needed to guide a variety of research and development projects. The engineering economic model contains five process plant programs: fish meal; biological; isopropyl alcohol extraction; press cake-biological; and press cake-isopropyl alcohol extraction. Process descriptions and flow sheets are presented in the next chapter.

Fish meal processing is a common operation and there are many such plants throughout the world. Fish meal is used for animal feed while

the other processes make products for human consumption. It was included to provide a basis for comparison and because frequently intermediate meal products are a starting point for the FPC processes. The other processes are viable candidates for commercial manufacture of FPC.

B. Cost Estimation

In the development and use of the model it is important to have accurate cost information. Equipment and capital cost data were obtained from a number of recent publications. These figures were compared and reviewed for consistency and accuracy. In several instances costs were adjusted to meet the actual experience of individuals knowledgeable in the field of marine protein manufacturing. Finally all costs were adjusted to the base of early 1970.

The adjustment of cost data from the past several years to an early 1970 value was made using the Marshall and Stevens Equipment Cost Index which is published in the periodical *Chemical Engineering*. The M & S Equipment Cost Index is based on a value of 100 in the year of 1926. The early 1970 base value of 297.5 is used for equipment costs in this report.

Adjustment in costs from one year to another is accomplished by multiplying the known cost by the ratio of the index values at the two years involved to obtain the desired cost. The choice of the M & S Index over several other indices that are available was based on the fact that the components used in the M & S Index are more nearly those present in FPC plants, and the general observation that all the indices have been moving at about the same rate in recent years.

Use of these indices over more than a few years leads to considerable uncertainty and is not recommended. It is hoped that users of the model will continually update the data from the best sources available and not resort to changing the cost index alone. Equipment is continually being developed and many specific items do not follow the average trends.

There is a wide variation in costs at any given time. This is due in part to the inventory and backlog situation of the individual manufacturers and suppliers. The best cost information is a written quotation for a specific item

to be purchased during a given period. In a number of instances, particularly for the IPA-Extraction process (17), quotes on equipment were available and were used in adjusting the literature data. Essentially the same thing was done, through discussions with experienced persons, for the typical fish meal process.

The capital cost estimating procedure of Guthrie (6) was used in developing the process engineering economic model. A module technique is employed in which cost elements having similar characteristics and relationships are grouped together. This grouping is discussed in the program output section. Published equipment cost information was obtained from a number of sources (6, 7, 8, 9, 10, 12, 13, 14, and 15). The cost data were fit to appropriate equations and are contained in the cost subroutine. This portion of the computer program and procedures for changing the data are discussed later in the report.

Costs of chemicals and raw materials were taken from recent issues of the *Oil, Drug and Paint Reporter* and from actual purchasing experience. Some of these are program input items and can be changed whenever the program is used. The cost of fish is quite varied and depends greatly on local conditions. Fish meal manufacturers often make contractual arrangements with the boat owners whereby the final price paid is dependent upon the income ultimately received from selling the fish meal. This input item will require close attention of the program user. The tradition of the industry of speaking in terms of fish rather than weight can also be a point of confusion. For menhaden, one million fish is taken to be 755,000 pounds of fish.

C. Process Economics

The model develops the construction, operating, and production aspects of each process subject to specific input and internal information. It does not deal with the economics of selling the products and the resulting profits and return on investment.

Each of the processes makes several products and consequently requires the managerial decisions of cost allocation to establish selling prices of products. Marketing, inventory management, product distribution, and sales con-

tracting are important factors in the final decision on commercial operation. The model is intended to provide processing information upon which preliminary deliberations and decisions of the venture risk type can be made.

It is most important in using the model to recognize its limitations. Of the processes in the model only fish meal processing is a commercial operation at present. Even in this case the model attempts only to give representative information for a somewhat typical kind of plant under average conditions in the United States. Several IPA extraction plants for FPC production are under construction. The model IPA process is based on a modified analysis of the National Marine Fisheries Service Experiment and Demonstration Plant at Aberdeen, Washington. In all other instances the processes are in the early pilot plant level of development.

The model is also generally limited to use for plants handling 50 or more tons per day of fish. Modern domestic fish meal plants handle 1,000 or more tons per day and it is expected that FPC plants will be in the range of 100 or more tons per day. There is significant interest in processing FPC on board ships and developing small village industry operations. Use of the model in the 10 to 50 tons per day range will require some modification or at least close attention and judgment about the details of the output.

The model is presently applicable to coastal plants. To place one of these processes on board a ship will require significant changes. Generally space is a limiting factor on board ship and the processes would need to be redesigned for compactness. Special modifications to the ship could be costly, while certain land operation requirements, such as pollution control, might be eliminated, resulting in savings.

Village industry operation, and operation in foreign countries in general, will require a number of changes. The model provides for modern, instrumented, continuously operating plants. Equipment costs are for the United States and, in general, the plants are custom-made large facilities. Smaller plants, in the 10 ton per day sizes, might be mass-produced and thereby benefit from unit cost reduction much like appliances. If the appliance approach is not used on-site fabrication of village level

plant would probably be of the batch type. Such plants would have additional difficulties with quality control. A training program for village plant operators might be necessary to overcome potential health and operating problems.

III. DESCRIPTION OF PROCESS MODELS

A. Fish Meal Process

The diagram of the fish meal plant is given in Figure 1. On the drawing, the streams are labeled. The fish are processed for three products, fish meal, fish oil, and fish solubles (50% water). An option is provided as to whether fish solubles are produced as a product or added to the fish meal.

Fish are unloaded from the boat by fish pumps. A weighing conveyor carries the fish to a storage unit which has a three-day capacity. A bucket conveyor takes fish from storage and drops them into a cooker. Oil is removed from the cooked fish in a continuous screw press.

The press cake leaving the press contains 50% solids. This stream in tons/day is labeled AA(91,2). The press liquor contains the oil and water from the fish and 15% of the total fish protein. It is labeled AA(91,3). The cookers are available in 100 ton/day and 250 ton/day sizes. Similarly two different sizes of screw presses are available. The selection of cookers, presses, and screens is internally handled in the program.

The program then branches to two processing streams. The stream containing most of the oil and water is discussed below. The first input option considered is whether to add the fish solubles streams to the fish meal stream [IPTION(1) = 2], or to market them as separate products, [IPTION(1) = 1].

From the presses, stream AA(91,2) passes through a mixer where the recycled fish solubles may be combined with the main stream. The stream then goes to steam tube drying in which approximately one-half of the weight is evaporated. Antioxidant, corresponding to 0.01 #/# of oil retained in the fish meal, is then added. The meal passes through a

mixer to a storage unit where it is cured for 15 days. The meal is milled prior to bagging.

Stream AA(91,3) is centrifuged. The centrifuge is sized from the flow in gallons/hour. The oil is then polished with hot water (10% of the oil weight of water is used) in a second centrifuge. The dummy variable TONSA is used for this stream at this point in the program. The fish oil product is designated AA(90,5). All hold tanks in the stream have a one-hour holding time. The fish oil storage capacity is 15 days.

The water and soluble protein are conveyed into an acid mix tank where it is mixed with sulfuric acid. This stream TONSWW then passes into a triple effect evaporator. The streams TONA and TONC are in tons/hr rather than tons/day. TONA is the inlet stream to the triple effect evaporator. TONC is the stream from the third effect going to the concentrator. The resulting fish solubles stream is 50% protein. It may be marketed as a product AA(90,4) or returned to the mixer and processed as fish meal. The storage capacity for fish solubles is 15 days.

In summary, three products may be produced—fish oil, fish solubles, and fish meal. Also, by an appropriate choice of option the fish solubles may be recycled and processed with the fish meal.

B. Biological Process

In the biological processes the proteins of the fish are partially hydrolyzed with enzymes to permit separation of the oil, bone, and proteinaceous material. The distinguishing feature of the process is large heated and stirred vessels into which the ground fish is fed and in which the digestion takes place. The sub-routine handling this process is labeled "Sub-routine Biolog"; the flow streams and equipment blocks of this subroutine are identified in Figure 2. In addition to the standard four-card input discussed in Section IVD, "Biolog" requires 5 input items which are entered on a fifth card in E12 format.

1. UNLOADING, STORAGE AND GRINDING

The handling of the fish up to the digester stage includes fish pumps, conveyors with wash

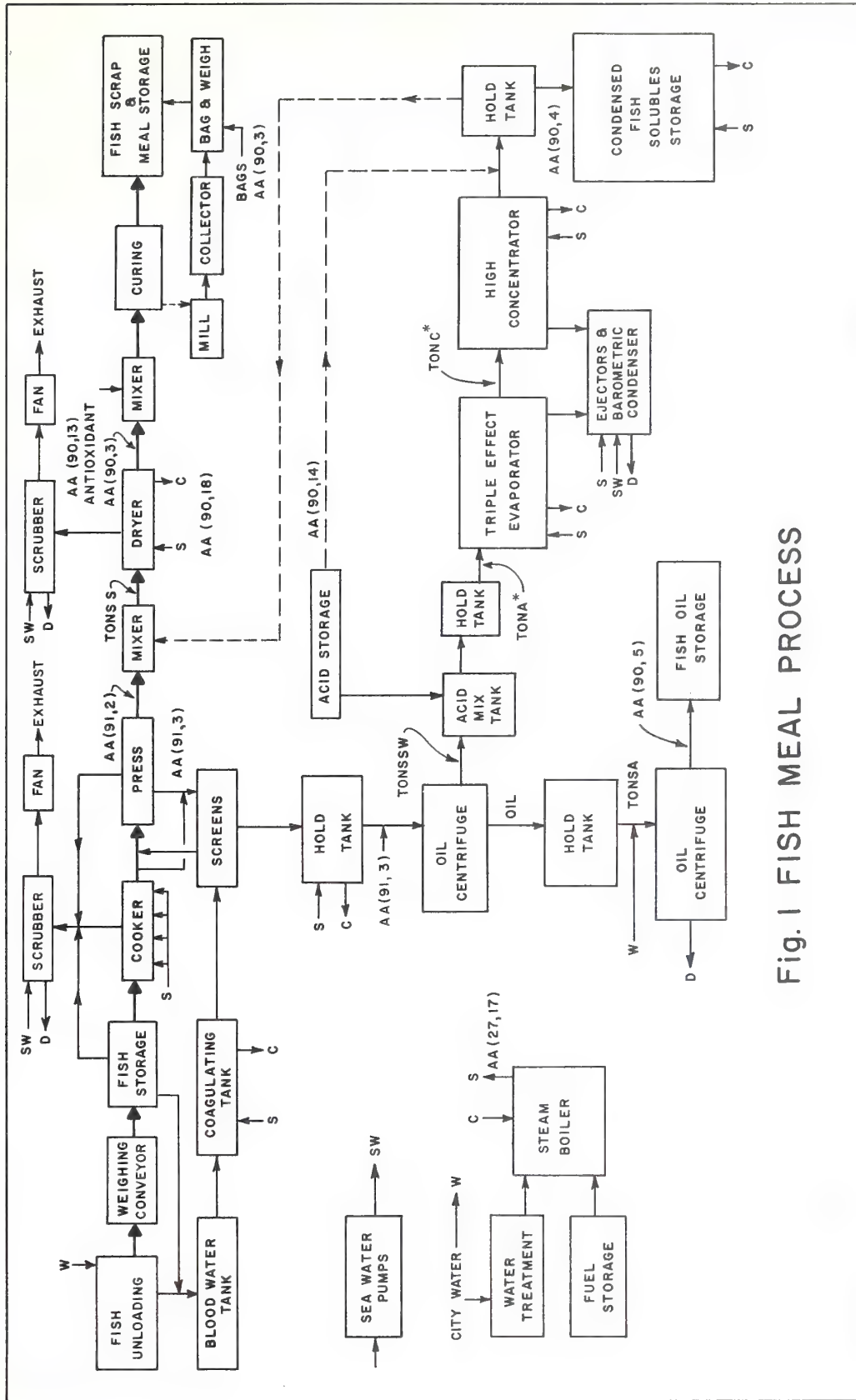


Fig. 1 FISH MEAL PROCESS

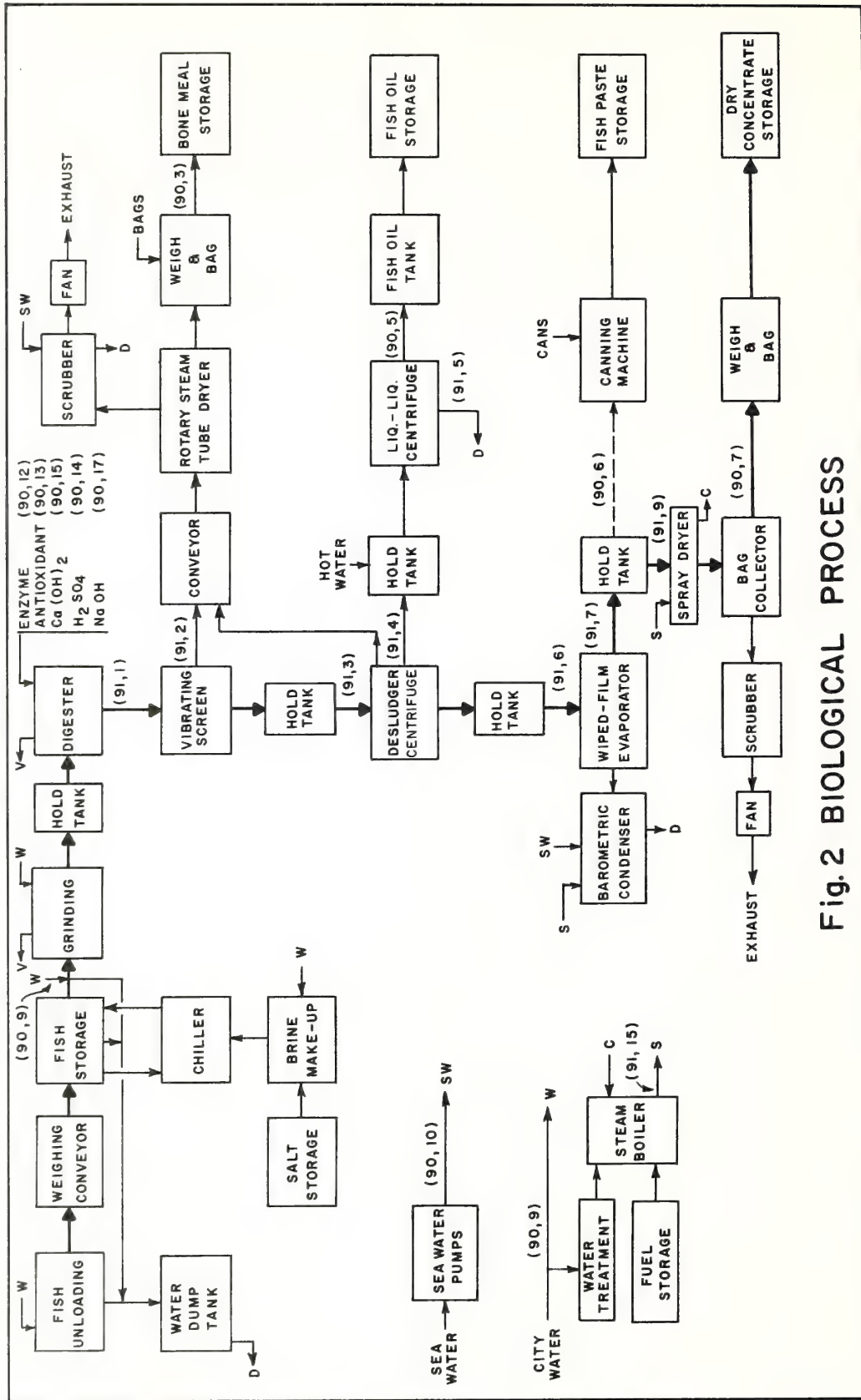


Fig. 2 BIOLOGICAL PROCESS

and weighing provisions, and refrigerated brine storage. Storage is an expensive equipment item and a capacity sufficient for 3 days of plant operation is assumed. From the refrigerated redwood bin the fish are taken by means of a bucket elevator to grinders. The ground fish is conveyed to the digesting vats.

2. DIGESTERS

The digesters are stainless steel, jacketed, and stirred vessels. They are sized for 5-hr residence time, with the assumption that each plant needs at least three vessels in order to provide a continuous feed to the equipment processing the digested stream. If a plant capacity exceeds three 10,000 gal. vessels, the number of vessels is increased. The streams feeding into the digesters besides the ground fish are 1) water, 2) enzyme, 3) CaOH, 4) 5N-NaOH, 5) antioxidant, and 6) conc. H₂SO₄. All of these streams have a separate identification in the AA(90,J) matrix (see Fig. 2); thus if processing conditions at the digester stage should change in the future, these changes can be made in sub-program "Biolog" without unduly affecting the other parts of the program. The program contains the following relationships between the streams:

- a water — equal in weight to ground fish feed.
- b enzyme — added in sufficient quantity to correspond with effectiveness (program input).
- c CaOH — 0.84% of the weight of the ground fish feed.
- d 5N-NaOH — 4.3% of the weight of the ground fish feed.
- e Antioxidant — 0.01% of the (oil & ash & protein) of the fish feed.
- f conc. H₂SO₄ — 1.9% of the ground fish feed (added after hydrolysis).

Digestion itself is a 5-hr batch process, but since at least 3 digesting vats are used per plant, the streams after the digesters are continuous. The digested fish slurry is fed by gravity into vibrating screens (one screen per digesting vat) for removal of bones and scales. The screened liquid is pumped to a self-cleaning disk centrifuge for separation of undigested solids and oil from the aqueous stream.

3. BONE FEED STREAM

The bone feed stream consists of the bones and scales removed from the vibrating screens (moisture content 50%) and the sludge discharged from the desludger centrifuge (moisture content 76%). The bone feed stream is conveyed into a stream tube dryer where the moisture content is reduced to 10%. The dry bone feed is sent to a hammer mill and then bagged. The final product stream [AA(90,3)] identified as "bone feed" is 40% protein, 22% oil, and 28% ash.

4. OIL STREAM

Approximately 75% of the lipid content of fatty fish is removed in the oil discharge from the disk centrifuges. Most of the balance of lipids is adsorbed on the undigested solids and removed in the sludge discharge. The oil stream from the centrifuges is pumped into intermediary storage tanks (with a maximum storage of one hour). About 10% additional hot water is added to the oil and the mixture is fed to "Sharples" type polishing centrifuges in which the water including solvated solids and blood are removed. The product fish oil can be stored up to 15 days and is sold in bulk.

5. DISSOLVED SOLIDS

Less than 1% of the total fish lipids are contained in the aqueous main stream discharge from the disk centrifuge. This stream is pumped to a wiped film evaporator in which the stream moisture content is reduced to 50%. This evaporator output stream is called "fish paste." Depending on the input option, all or part of it is either packaged in cans or fed into a spray dryer where the moisture content is further reduced to 5%. The exit stream from the spray dryer is bagged as the "dry concentrate" product. The fish paste product is 41% protein, 0.3% oil, and 8.3% ash. The dry concentrate is 79% protein, 0.5% oil, and 16% ash.

C. Press Cake-Biological Process

This process (Figure 3) is similar to the Biological process. The differences are that be-

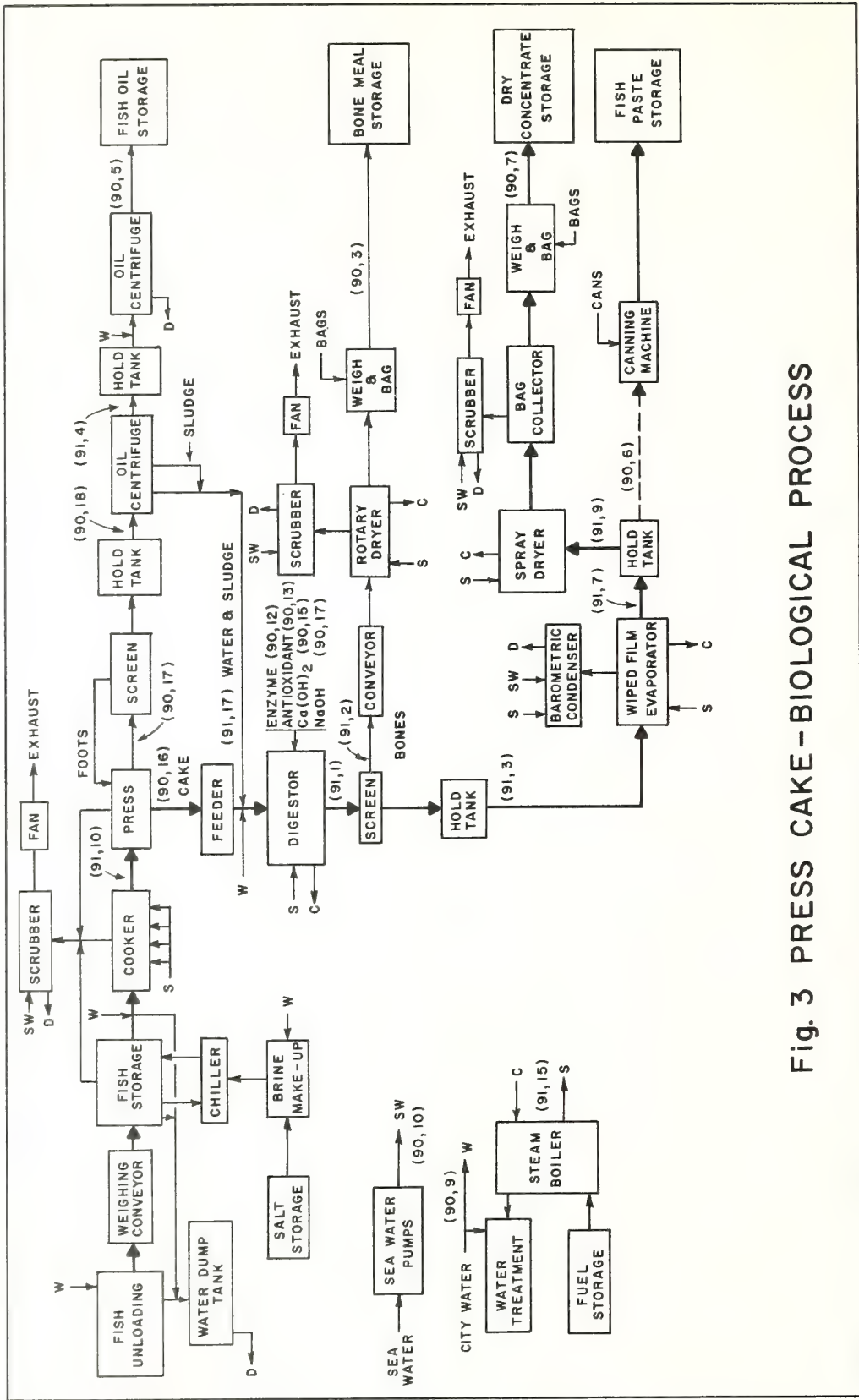


Fig. 3 PRESS CAKE - BIOLOGICAL PROCESS

fore being fed to the digestion vats the fish are cooked and pressed as in the Fish Meal Process. The separation of oil and stick water takes place before rather than after the digestion stage. Process description: a) Input (besides the standard input) is the same as for the Biological process, except that in this case the enzyme which is added to the digester is based on 100 lb. of cooked and pressed fish (referred to as press cake) rather than on raw ground fish; b) Unloading and storage processes include fish pumps, conveyors with wash and weighing provisions, and refrigerated brine storage for up to 3 days of plant operation. The stored fish is lifted by bucket elevators into steam cookers. The fish are cooked and pass into screw presses where the moisture content of the "press cake" is reduced to 60%.

The press liquor is screened and pumped from a hold tank to a centrifuge for oil separation and "foots" removed by screening are recycled to the press. The separated oil is polished with hot water in a second liquid-liquid centrifuge, as in the Biological process, and pumped to bulk storage.

The aqueous "stickwater" stream from the first centrifuge contains both soluble and insoluble solids. It is added to the press cake in the digesting vats along with additional water to form a press cake slurry for enzymatic hydrolysis. For hydrolysis with the alkaline enzyme the pH is adjusted with 5N NaOH at 2.2% of the weight of raw fish feed.

After a 4-hr hydrolysis the slurry is passed through a vibrating screen. Bones and scales with a 50% moisture content are conveyed from the screen to a stream tube dryer where the moisture content is reduced to 10%. The dry bone meal is sent to a hammer mill and then bagged.

The screened hydrolysate is concentrated to a fish paste containing 50% solids in a wiped film evaporator. Depending on the input option, all or part of it is either packaged in cans or fed into a spray dryer where the moisture content is further reduced to 5%.

The final products are bone meal (36% protein, 9.7% oil, 47.4% ash), fish paste (39% protein, 6% oil, 5% ash), dry concentrate (75% protein, 11% oil, 9% ash) and fish oil. Insoluble solids are not removed by centrifuga-

tion as in Biological process.

D. IPA Extraction Process

The IPA process is shown in Figure 4. This is a solvent extraction process in which water and lipids are removed using isopropyl alcohol (17). Solvent recovery and recycle is an important part of the process. The first decision variable is whether wet deboning or no deboning is used. In wet deboning the bones are dried, ground in a hammer mill, packaged and sold as bone meal. This option is activated when IPTION(1) is equal to one. If no deboning is desired, no option is specified. In this case, the dried concentrate product will contain both protein concentrate and bone meal.

Unloading and storage processes include fish pumps, conveyors with wash and weighing provisions, and refrigerated brine storage for 3 days of plant operation. The ground fish is pumped to a slurry mix tank where solvent miscella M-2 is added. The solids go through four stages of extraction. They are separated from the miscella between stages by screens and presses.

For the material balance on the extraction vessels the miscella stream are designated STRMM(I) where I is the stage number. The constituent streams of oil, protein, ash, water, and isopropyl alcohol are designated STRM(I, J). Here, however, the index I designates the stream entering the Ith stage or leaving the I + 1 stage. The unit operation of this part of the process is a 4-stage liquid-slurry extraction process in which an azeotrope of isopropyl alcohol and water is used as the extractive solvent. The solvent to fish ratio is 2:1.

1. FISH PROTEIN CONCENTRATE STREAM

The slurry stream leaving the fourth stage of extraction contains the ash, most of the protein, and a small residual amount of oil. This stream enters a series of dryers (dryer, stripper dryer, and conditioner) in order to reduce the moisture of the stream to approximately 8% and to reduce the IPA residual to below 250 ppm. The amount of material leaving the conditioner is designated TASB. The fraction

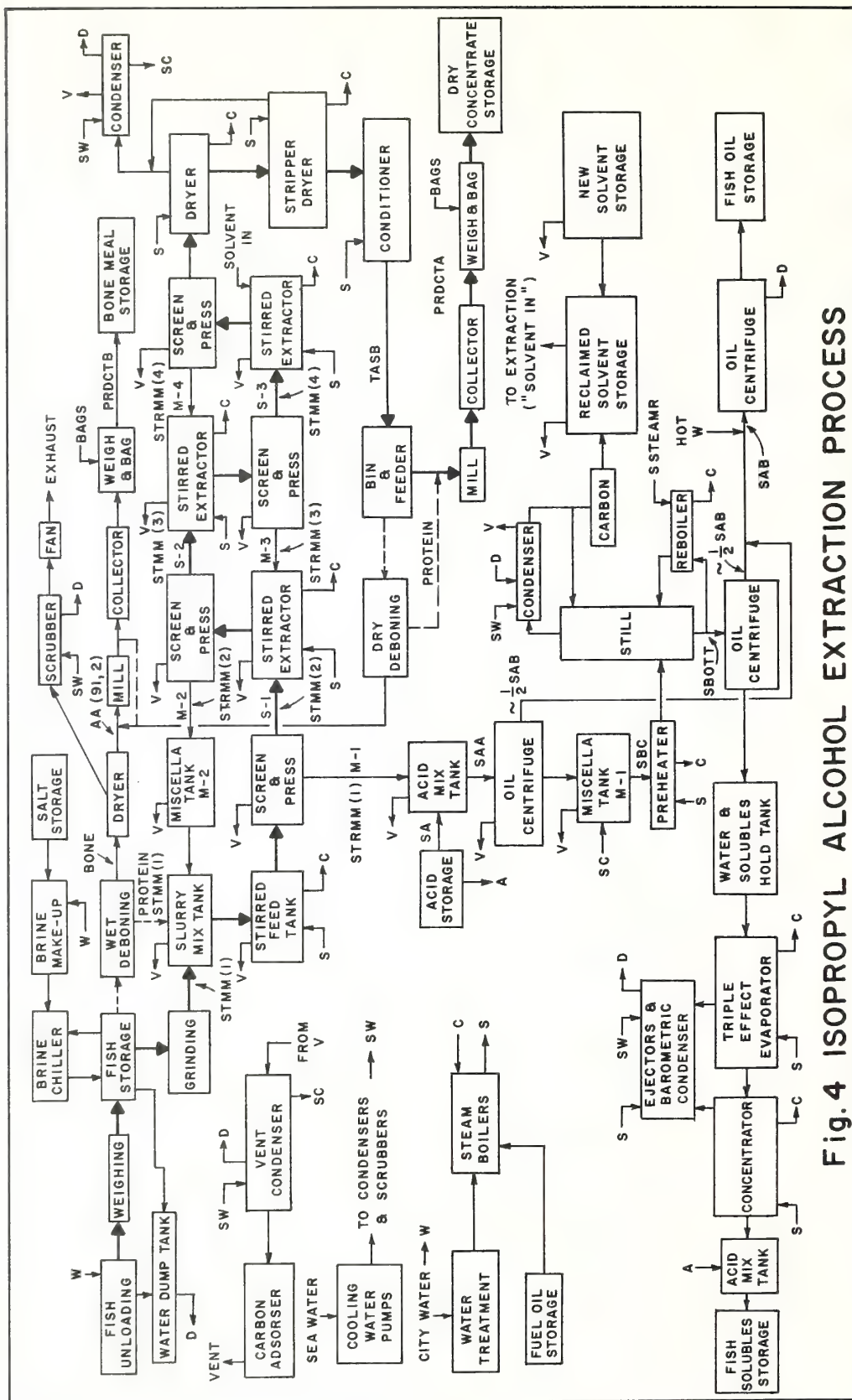


Fig. 4 ISOPROPYL ALCOHOL EXTRACTION PROCESS

of protein retained in the fish protein concentrate is designated as ZA7 and the amount of bone meal in the FPC is ZA8. The original fractions chosen are 0.96 and 0.04 respectively. They can be changed readily without affecting the main body of the program. The finished concentrate and bone meal are then milled and packaged.

2. OIL STREAM

The stream containing the bulk of the oil is the miscella stream leaving the first stage. This stream is acidified (conc. H_2SO_4 at 1.9% of fish feed) and enters an oil-water centrifuge. Approximately one-half of the oil is removed. This oil plus the oil from the still bottoms product, which was centrifuged, are combined into one stream. About 10% hot water is added to this stream before it enters a polishing centrifuge. This oil can be stored up to 15 days and is sold in bulk.

3. SOLVENT RECOVERY

The rest of the oil and solvent from the first oil-water centrifuge is heated prior to the distillation process. The solvent, which is mostly isopropyl alcohol, is distilled in a 25-tray column. SBOT(I) designates the constituent bottoms consisting of isopropyl alcohol, water, oil, and soluble protein. The product at the top of the column is designated STOP (I) and consists of isopropyl alcohol and water. The recovered solvent is then pumped to the storage tank where make-up isopropyl alcohol is added as needed.

4. FISH SOLUBLES

The non-oil portion of the centrifuged column's bottoms is fed to a triple effect evaporator. The product is further concentrated to 50% protein in a concentrator evaporator.

The products stream consists of fish protein concentrate AA(90,7), bone meal AA(90,3) (if wet deboning is specified), fish oil AA(90,5), and fish solubles AA(90,4).

E. Press Cake--IPA Process

The Press Cake-IPA process combines the proved technology of IPA extraction with a pre-processing of the raw fish in order to provide a more concentrated and more easily stored feed. A diagrammatic representation of the process is shown in Figure 5.

1. UNLOADING, STORAGE, AND PRESS CAKE PRODUCTION

The fish is unloaded by means of fish pumps, weighed and washed and stored in refrigerated brine. A storage capacity sufficient to provide 3 days of feed to the press cake production unit is provided. From the brine storage vat the fish is lifted by bucket elevators into steam cookers. The fish is cooked, crushed, and passes into a screw press which reduces its moisture content to 60%. The excess liquid passes through a vibrating screen filter into a hold tank. This liquid is processed separately in order to recover the oil and dissolved solids. The compressed bulk fish, called "press cake," is ground, transported by screw conveyors either into a closed redwood bin for intermediate storage in IPA or directly into the IPA extraction stages. The capacity of the intermediate storage is sufficient to provide a 50-day backlog for the IPA extraction portion of the plant.

2. IPA EXTRACTION

The press cake is turned into the final FPC product through multistage countercurrent IPA extraction. The program is set up in such a way that the number of extraction stages and their individual efficiencies can be changed readily. The standard number of stages is assumed to be four; however, any number up to eight can be specified in the input. If the desired number of stages is *other than four*, that number should be entered in column 40 of the first input card.

After each separation stage a detailed material balance on each component of the input-output streams is performed. The separation efficiencies for each component and each stage can be specified separately. They are stored in the library subprogram LIBRE and can be

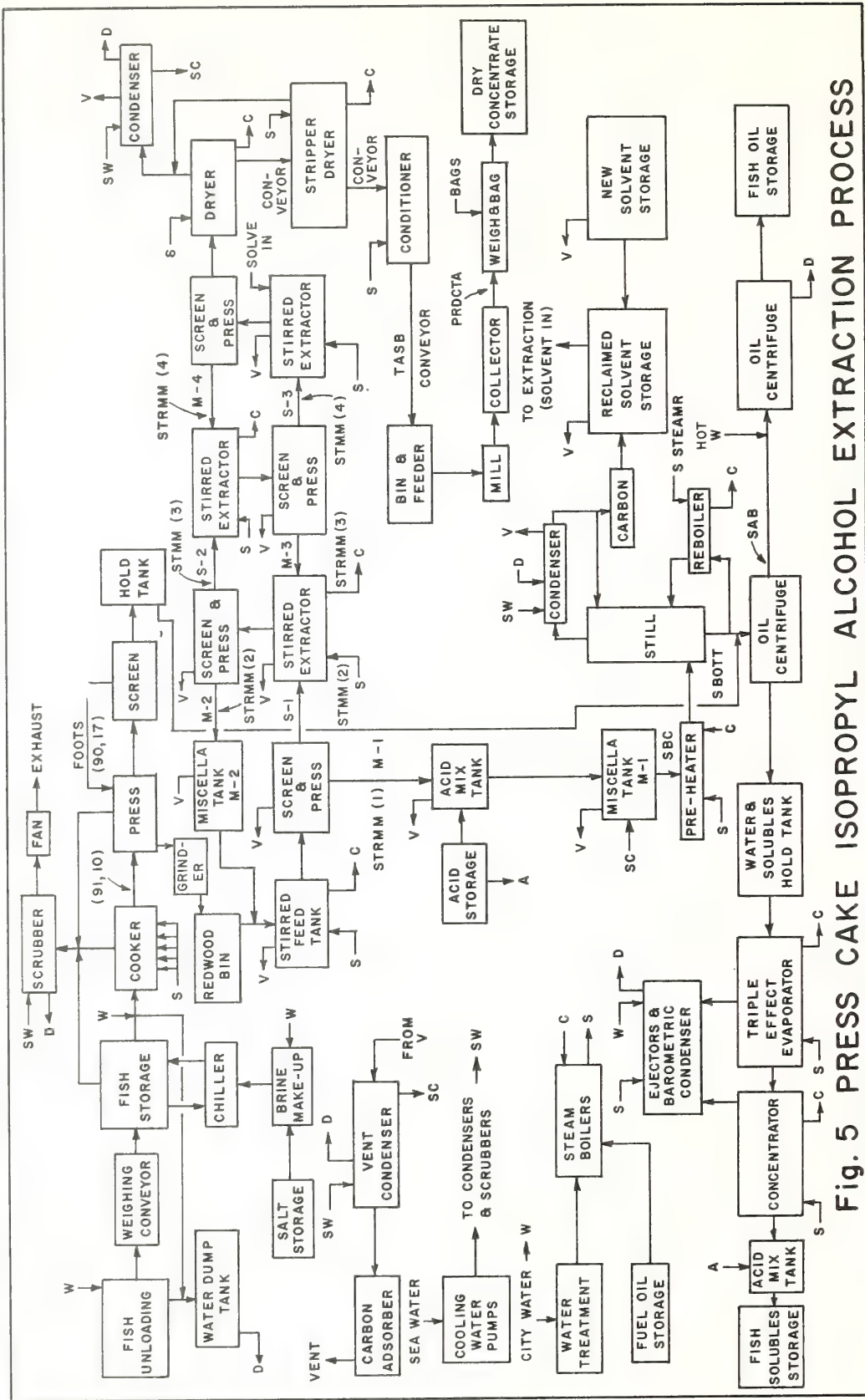
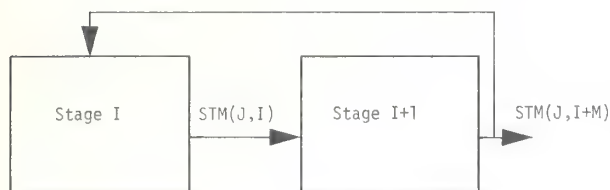


Fig. 5 PRESS CAKE ISOPROPYL ALCOHOL EXTRACTION PROCESS

changed readily without modifying the main program.

Consider two sequential stages I and I + 1:



The J index describes the five main components of the stream. The relationship is as follows:

- J = 1 — Oil
- J = 2 — Protein
- J = 3 — Ash
- J = 4 — Water
- J = 5 — IPA

The quantity for each component exiting from stage I + 1 is computed by the following relationship:

$$STM(J,I+1) = STM(J,I) * DATB(I,J)$$

Where: 1-DATB(I,J) is the extraction efficiency for component J in the I + 1 stage. These quantities are thus stored in the readily accessible LIBRE subprogram.

The above definition has to be modified for the case of the IPA content leaving the first extraction stage. The modification is:

$$STM(5,1) = STM(4,1) * DATB(1,5)$$

3. FISH PROTEIN CONCENTRATE STREAM

The slurry stream leaving the final extraction stage contains the ash, most of the protein, and a small residual amount of oil. The stream enters—in sequence—a dryer, a stripper dryer, and a conditioner in which its moisture content is reduced to about 8% and the IPA residual falls below 250 ppm. The solid stream leaving the conditioner is labeled TASB. It is milled, weighed, and packaged.

4. OIL STREAM

The stored liquid from the press cake production process and the still bottoms from the solvent recovery still are fed into a liquid-liquid

centrifuge. Oil separation efficiency is assumed to be 94%. Bottoms containing the dissolved solids are fed into a storage tank in order to be processed through evaporators, the top oil containing fraction is pumped into a polishing "Sharples" type centrifuge. Here 10% volume fraction of hot water is added. The purpose of this centrifugation is to remove entrained blood and remaining solids. The polished oil is fed into final oil storage tanks. A storage capacity sufficient for 15 days production is designed.

5. FISH SOLUBLES

The stream containing dissolved solids from the liquid-liquid oil separation centrifuge is fed into a triple effect evaporator followed by a concentrator. The moisture content is reduced to about 50%, the product is acidified and stored as fish solubles.

6. SOLVENT RECOVERY

The solvent-containing stream is preheated and passed into a 25-tray distillation column. The bottoms of the column pass, as noted, into the liquid-liquid centrifuge of the oil separation stream, the solvent-containing tops go through a charcoal filter and, after addition of requisite amounts of makeup solvent, are recycled to the IPA separation stages.

IV. COMPUTER USER INFORMATION

A. Program Outline

The programs making up the FPC cost analysis code can be divided into three classes.

- 1 Programs handling input and output data and performing calculations which are common to all FPC production processes. This class includes the MAIN program and the subprograms MATER, CAPTOL, and OPERAT.
- 2 The programs describing each of the five separate processes. The main portion of the computations is performed by these programs. The material and energy balances are computed. On the basis of this information and on

built-in decisions regarding equipment sizes (see Section B) the required capacity for the major equipment items are calculated. The six programs in this class and the process which they analyze are:

<i>Program Name</i>	<i>Process</i>
FPCXXI	Fish meal plant
BIOLOG	Biological process
PRESCK	Press cake biological process
XXIPA	Isopropyl alcohol extraction
PRSIPA	Press cake-IPA extraction process

3 The service and information subprograms. These consist of a large number of largely similar subprograms which calculate the cost for individual equipment items and of the library subprogram LIBRE which contains all of the costing data. The costing subroutines are discussed in more detail in Section C. Usually they are named directly by the equipment name and given an equipment capacity return, its cost and the cost breakdown. In some cases similar types of equipment are handled by single subroutines. The list of the equipment subroutines is:

<i>Identification Number</i>	<i>Equipment</i>	<i>Sub-routine Name</i>
6 =	Conical Hopper	Hopper
7 =	Fish Storage	Silo
8 =	Scrubbers	Conden
11 =	Pulveriser	Pulver
17 =	Screw Conveyor	Screwr
18 =	Hammer Mill	Hammer
19 =	Drum Dryer	Dryer
20 =	Pan Dryer	Deyerp
21 =	Rotary Vacuum Dryer	Dryerr
27 =	Boiler	Boiler
30 =	Spray Evaporator	Evpspr
31 =	Wiped Film Evaporator	Evpflm
32 =	Forced Circulation Evaporator	Evpfrc
33 =	Vertical Evaporator	Evphor
40 =	Shop Fabricated Tank	Storag
42 =	Pressure Vessel	Vessel

43 =	Distillation Column	Column
49 =	Jacketed Reacting Vessel	Reactr
50 =	Fish Grinder	Grinder
51 =	Vibrating Screen	Screen
52 =	Sharples Centrifuge	Sharp
53 =	Solid Bowl Centrifuge	Bowl
54 =	Vertical Basket Centrifuge	Cntfge
57 =	Free Flowing Solvent Blender	Blendr
65 =	Reciprocal Pumps	Pmprec
66 =	Centrifugal Pumps	Pmpent
67 =	Shell-Tube Heat Exchangers	Heatex
70 =	Belt Conveyor	Belt
71 =	Bucket Conveyor	Bucket
72 =	Scale	Scale
73 =	Agitator-Propeller	Agitor
74 =	Ball Mill	Balmil
75 =	Bagging Machine	Baggma
78 =	Rotary Drum Filter	Filter
80 =	Overhead Crane	Cranes
81 =	Drag Conveyor	Dragma
85 =	Mechanical Refrigeration	Refrig
99 =	Facilities	Fascil

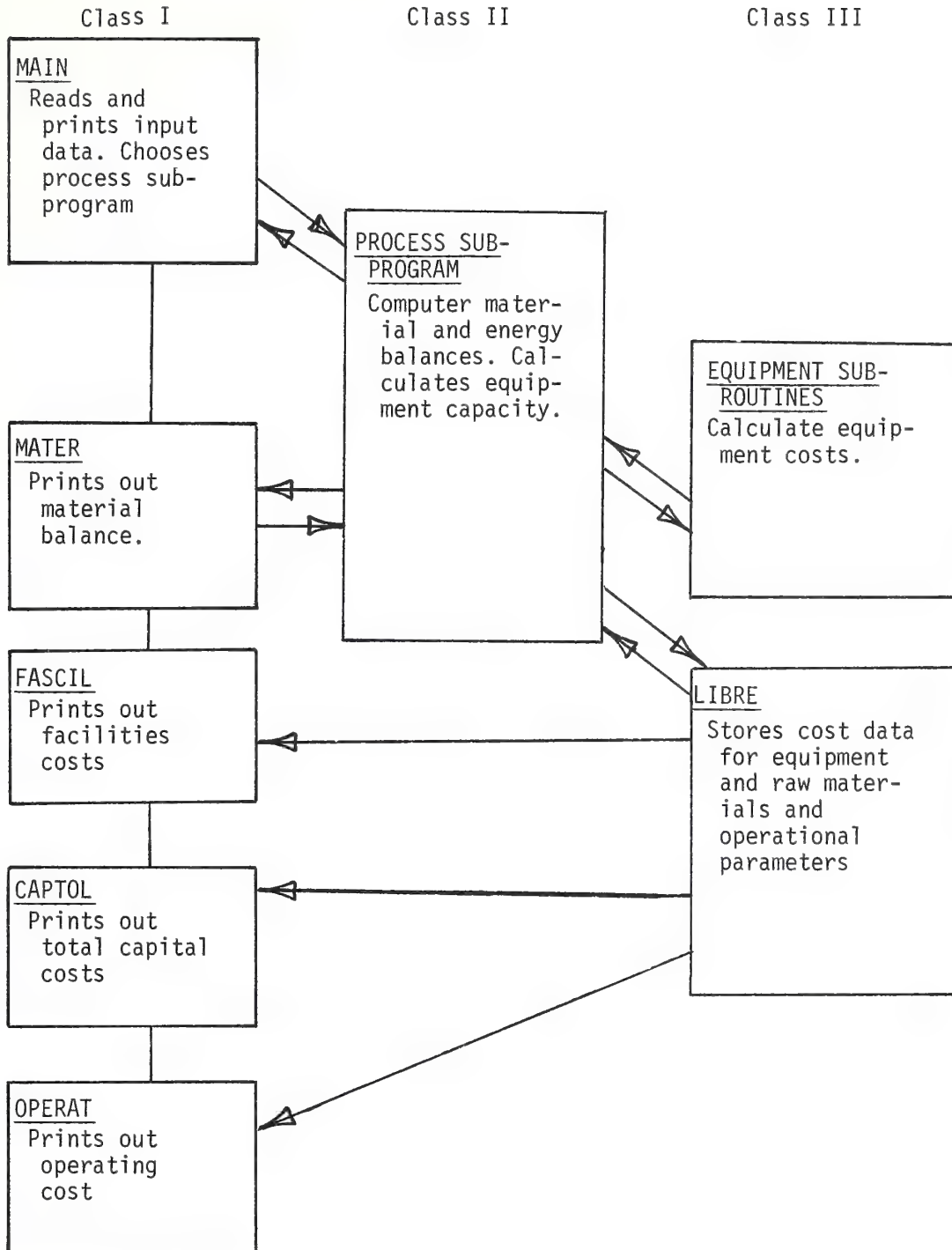
The library program LIBRE performs no other function besides storing the cost data for all equipment items and those process raw materials which are not given in the input data. These data are made available to all the subroutines by reading the contents of LIBRE into a large common block which is made up of two rectangular matrices and a linear matrix, namely AA (100,20), IA (100,5), and BB (100). The first index of the AA and IA matrix usually refers to the identification number of specific equipment items. The BB matrix contains raw material cost data. Thus LIBRE has to be called just once for each individual cost calculation. This is done from the MAIN program.

Most of the program changes which will be necessary as cost data change or become more accurately known can be done in LIBRE. This is discussed in more detail in Appendix A.

The interrelationship of programs during a typical calculation is shown diagrammatically in Figure 6.

Figure 6

Simplified Flow Diagram for the
FPC Cost Analysis Program



B. Equipment Sizing

This section follows the listing of equipment in subroutine LIBRE. Only those items of equipment about which design decisions had to be made are discussed.

Pulp Presses are 6 feet long and the diameter in inches is calculated by the relation $8(\text{ton-days}/50)^{1/2}$ up to 24.

Screw Presses (for fish meal) are in two sizes with preference for the large one. For 250 ton-days the size is 21 feet long and 16 inches in diameter and for 100 ton-days, or less, the size is 15 feet long and 12 inches in diameter.

Rotary Steam Tube Dryers are sized according to amount of feed based on 2.5 square feet to process one ton-day of material fed per day.

Cookers are based on 0.25 square feet per ton-day of fish.

Boilers are based on 150 psig steam and sized in terms of 1.05 times required steam for the entire process.

Spray Dryers are sized on pounds of water to be evaporated as given in reference 7.

Wiped Film Evaporators are based on $\Delta T = 50^\circ \text{ F}$ and $U = 500 \text{ BTU/hr ft}^2 \text{ }^\circ \text{ F}$ giving the relation area in square feet equal pounds of water evaporated per hour divided by 25.

Forced Circulation Evaporators are based on $\Delta T = 50^\circ \text{ F}$ and $U = 400 \text{ BTU/hr ft}^2 \text{ }^\circ \text{ F}$ giving the relation area in square feet equal pounds of water per hour evaporated divided by 20.

Vertical Tube Evaporators are taken as (a) three in series with $\Delta T = 50^\circ \text{ F}$ and $U = 400 \text{ BTU/hr ft}^2 \text{ }^\circ \text{ F}$ giving the relationship area in square feet equal pounds of water evaporated divided by 20, or (b) the concentrator evaporator which has $\Delta T = 50^\circ \text{ F}$ and $U = 500 \text{ BTU/hr ft}^2 \text{ }^\circ \text{ F}$ giving the area in

square feet equal to the pounds of water evaporated divided by 25.

Storage Tanks are based on the holding time for the stream involved.

Distillation Columns are prorated from the Experiment-Demonstration Plant (EDP) still design and directly scaled. Stage number is 25, height is 54 feet and reflux ratio is two as they are in the EDP. The diameter of a still cannot be less than 4 feet and increases in 2-foot intervals of diameter (4, 6, 8, etc.).

Reactor Vessels (biological) are sized based on a residence time of 5 hours. The minimum number of vessels for a plant is three. The maximum vessel size is 10,000 gallons.

Fish Grinders are in two sizes for 150 and 75 ton-days with preference for the larger size. Horsepower requirements are based on 40 Hp/3 tons/hr throughout.

Centrifuges are of two types. Solid-liquid (disk-type slimers) having 2000 gallons per hour of throughput, and liquid-liquid (Sharples) having 1000 gallons per hour capacity. In both cases only one size is used and it requires 20 horsepower.

Pumps, both centrifugal and reciprocating, are sized in terms of the product of gallons per minute times the required pressure in psi, generally taken as 30 psi.

Heat Exchangers are of two kinds. Heaters using steam are sized according to area in square feet equals 0.1 times pounds of steam required, ($\Delta T = 20^\circ \text{ F}$ and $U = 500 \text{ BTU/hr ft}^2 \text{ }^\circ \text{ F}$ and the cooling water rise is 20° F).

Belt Conveyors are taken as 100 feet long. For less than 150 ton-days the width is 36 inches and for greater than 150 ton-days the width is 48 inches.

Bucket Conveyors are based on a lifting height of 20 feet.

Agitators are for two purposes. For slurries the required horsepower is 0.01 times the tank volume in gallons. For waterlike liquids the horsepower is 0.005 times the tank volume in gallons.

Bagging and Packaging Machines are based on bags or cans per minute. 100-pound bags are used for fish meal, 25-pound bags for FPC and other dry products, and 5-gallon cans for paste products.

Refrigeration includes brine recycle pump and heat exchanger and is based on 0.5 tons of refrigeration per ton of fish stored and three days of fish storage.

Brine make-up — This is a unit called a Brinopac, which delivers 50 gal/hr of 100° brine. It is 24 inches in diameter. The price FOB with hopper is \$1,190. This unit is good for any plant up to 300 ton-days. For any larger plant, the unit would cost \$1,880.

Boiler Feed Water Treatment — This includes all the material to purify the boiler feed water, i.e., the water in the make-up tank is deaerated to get rid of dissolved O₂ and CO₂. Ion exchange is used to eliminate Mg and Ca ions. A pH adjustment is also made. The initial unit for boiler feed water treatment for any size is about \$1,000. After that, it costs \$100/month for upkeep.

Buildings are sized at 14 square feet of ground floor per ton-day of fish. Generally buildings are 40 feet high and have several levels depending on operations.

Real Estate is based on 0.0050 acres per ton-day of plant capacity.

Warehouse space is taken as 15 square feet per ton-day for fish meal plants and 3 square feet per ton-day for other plants.

Fish Pumps are reciprocating type. The plants use one fish pump for each 500 ton-days of fish. Smaller plants have one pump.

Dock Facilities are 2,400 square feet for each fish pump.

C. Equipment Subroutine

The material base cost of almost all pieces of equipment are estimated by the equation

$$\text{Base Cost} = a (\text{SIZE})^b \quad (1)$$

The installation cost, labor cost, and incidental costs are determined by

$$\text{Subsidiary Costs} = (\text{Base Cost}) \cdot d^i \quad (2)$$

where d = cost factors in LIBRE, $i = 1, 2, 3, 4$.

The subprogram associated with the fisheries costing programs uses the following variables:

COST (1)	Base Cost
COST (2)	Field Materials Cost
COST (3)	Labor Cost
COST (4)	Indirect Cost
COST (5)	Total Cost
COST (6)	Uncertainty in Cost

The base cost is updated by multiplying the value determined in equation (2) by the Marshall and Stevens index BB (1).

The factors accounting for materials cost, labor cost, indirect cost, and uncertainty cost as well as the constants a and b are stored in program LIBRE.

The factors are:

AA (IX,7)	= Unit Cost (a)
AA (IX,8)	= Exponential in Cost Equation (b)
AA (IX,11)	= Materials Cost Factor
AA (IX,12)	= Direct Cost Factor
AA (IX,13)	= Indirect Cost Factor
AA (IX,14)	= Uncertainty Cost Factor

In a limited number of the subprograms, the factor a depends on a second size variable. In this case the cost is entered directly into the subprogram:

i.e. SCREWR

Furthermore, in some cases, it is desired to have a materials option. Several approaches have been used in the program:

i.e. PMPCNT
STORAG

In subsequent changes it is recommended that the following procedure be used. The material is selected in the program and designated by IA (IX,5)=INTEGER. For example if the equipment is to be constructed of monel then IA (IX,5) = 8: it is not necessary that the integer be associated with the same material for each item of equipment. In the subprogram one has the statements

```
IF (IA (IX,5). EQ. 8) BB (2) = 6.1
COST (1) = COST (1) * BB (2)
```

The second card comes after the computation of the indirect, labor, and materials cost based on the initial base cost.

The factor BB(2) can be entered from the main program (XXIPA, BIOLOG, etc.) as well. In addition a print statement is added to be consistent with the new option.

Usually the sizing equation is adequately represented by one sizing variable. This term is designated AA (IX,17). Occasionally it is necessary to have two variables, in which case the variable is usually AA (IX, 18), although on occasion AA (IX,20) has been used.

To illustrate the costing program we consider a typical subprogram BUCKET, the program for the bucket conveyor.

SUBROUTINE BUCKET*

1. IX + 71
2. Q = AA (IX,7)
3. IF (AA (IX,18). GR. 30. and. AA (IX, 18). LE. 75),
AA (IX,7) = AA (IX,7) + 180
4. IF (AA (IX,18). GR. 75.) AA (IX,7) =
AA (IX,7) + 280.
5. COST (1) = AA (IX,7 * AA (IX,17)
** AA (IX,8) * BB (1)
6. COST (1) = COST (1) * .001

* FORMAT, DIMENSION, PRINT, common statements have been omitted.

7. COST (2) = COST (1) * AA (IX,11)
8. COST (3) = COST (1) * AA (IX,12)
9. COST (4) = COST (1) * AA (IX,13)
10. COST (5) = COST (1) + COST (2) +
COST (3) + COST (4)
11. COST (6) = COST (5) * AA (IX,15)
12. DO 1 I = 1,6
13. 1 COST A (I) = COST A (I) +
COST (I)
14. AA (IX,7) = Q

Statements 2 and 14 are necessary in order that the values in LIBRE remain constant when the subroutine is used repeatedly.

Statements 3 and 4 adjust the value of the constant *a* [AA (IX,7)] for different values of AA (IX,18) which is the capacity of the conveyor in tons. The size unit AA (IX,17) is the height in feet.

Statements 5 and 6 determine the base cost in thousand dollar groupings. In 7-11 the costs of materials, labor, incidentals, and cost variation as well as total cost are determined.

In statements 12 and 13 the running cost of the plant option (IPA, Biological, etc.) is computed.

If different materials of construction were used then one would add the statement

$$\text{COST (1)} = \text{COST (1)} * \text{BB (2)}$$

between statements 9 and 10.

D. Program Input

The input to the FPC program can be divided into two parts: a) the "standard" input which is common to all of the different processes; b) the "optional" input presented in Section III, which discusses the individual processer; here we shall explain the standard input.

The standard input consists of four cards. The first of these enters integer input data, the remaining three enter input data in the floating point format.

<i>Program Variable</i>	<i>Columns</i>	<i>Description</i>
I. Card 1:	Format: (8I10)	
A. Iz	1-10	Fixes process to be analyzed. 1 = fish meal 2 = IPA 3 — biological 4 = press cake — biological 7 = press cake — IPA extrac- tion
B. Options	11-20	
1. fish meal IPTION(1) IPTION(2)		1 = solubles are product 2 = solubles recycled
2. IPA IPTION(1)		1 = wet deboning blank = no deboning
II. Card 2:	Format (3E 12.5)	
tons	1-12	The tons of fish to be processed per day.
BB(1)	13-24	The Marshall-Stevens index tak- ing the 1970 index of 297.5 as one.
BB(50)	25-36	The operating days per year.
III. Card 3:	Format (5E 12.5)	
BB(5)	1-12	Cost of the fish in ¢/lb.
BB(6)	13-24	Cost of electricity in ¢/KWHr.
BB(7)	25-36	Labor and supervisory costs in dollars/hr.
BB(8)	37-48	Depreciation and interest in per- cent per year.
BB(10)	49-60	Fuel cost in dollars per therm.
IV. Card 4:	Format (3E 12.5)	
BB(30)	1-12	Oil composition of the fish in weight percent.
BB(31)	13-24	Protein composition percent.
BB(32)	25-36	Ash composition in percent.
V. (For Biological and Presscake programs only)		
Card 5:	Format (5E 12.5)	
BB(40)	1-12	The effectiveness of the enzyme being used in lbs. of enzyme re- quired per 100 lb. of fish being processed. (For press cake Biological, it is per 100 lb. of press cake being processed.)
BB(41)	13-24	Price of enzyme is \$/lb.

BB(42)	25-36	The percentage of the total dissolved solids stream coming out of the wiped film evaporator (see Figure 2) which is packaged in paste form.
BB(43)	37-48	The effectiveness of the antioxidant being used, in lbs. of antioxidant required per 100 lb. of fish or 100 lb. of press cake.
BB(44)	49-60	Price of antioxidant in \$/lb.

VI. (For Press cake — IPA extraction only)

Card 1:	Format (8I10)	
	40	The number of IPA extraction stages (if different than four) should appear.

E. Program Output

The output of the cost analysis program is presented in seven separate sections:

- 1) Printout of input data.
- 2) Detailed equipment costs.
- 3) Material and energy balance.
- 4) Cost of facilities.
- 5) Capital costs.
- 6) Operating costs.
- 7) Production Cost of FPC.

Each of these sections is printed out in the form of a table. The contents of these tables will now be taken up in turn.

1) *Input Data*.—Identifies the process being analyzed, prints out all of the external input data and operating options.

2) *Detailed Equipment Costs*.—This is the most extensive table of the output. It presents the total cost and the cost breakdown of each major item of equipment required in a given process. Each equipment item is identified, its capacity, capacity units, and major construction material is printed. Following this information the total cost and the cost breakdown for this equipment are given. The cost breakdown uses the scheme of Reference (6) which is identified in the table headings. That is,

the first column labelled "Base Cost" gives the FOB. to manufacturer cost for this type and capacity equipment. This cost is multiplied by the Marshall and Stevens index given in the input data. The methods used computing this cost, the sources of the required internal data and the means for modifying these data are presented in Appendix A.

The subsequent three columns present additional costs which are incurred before the purchased equipment becomes operable.

Column 2, the "Material Costs" includes such diverse items as piping, electrical wiring, equipment base, and heat insulation. Column 3, the "Labor Costs" are the labor costs incurred during installation, and Column 4, the "Indirect Costs", summarizes remaining expenses such as shipping, insurance, construction overhead, and construction engineering costs.

All of these cost items are calculated as factors of the first column. These factors vary with equipment type but not with capacity. For each equipment item they are tabulated in the subprogram LIBRE and are easily accessible for modification.

The fifth column, titled "Module Cost", is a summation of the four previous columns and represents the capital investment required to design, order, ship, and install a given equipment item. Finally, the last column, titled "Range", is an estimate of the reliability of

these cost figures. This estimate is based upon the cost data available at the end of 1969 and summarized in the LIBRE subprogram. As time passes and cost figures are modified, the range estimate should be changed as well.

The information described above is printed out individually for each major piece of equipment even if multiple items of identical type and capacity of equipment are required. The sequence of printing out this information starts with equipment required to unload and store the fish (that is, the first item is always the fish pumps), and after that follows the main process streams. For example, in the fish meal plant analysis the equipment required to process the solids stream is presented first, then come the centrifuges required for oil separation, the evaporators required to concentrate the dissolved solids, and finally equipment items which do not really fit into the process stream, as the boiler, fork lift, or the cost of the instrumentation loops.

3) *Material and Energy Balance.*—This table presents first the overall, then the detailed material and energy balance. In the overall section of the table the total steam, electricity, and cooling water used in the process is given. The fish feed is broken down into the oil, protein, and ash components.

The detailed portion of the table prints out the process stream balances in terms of hourly throughput. The sequence of printout generally follows the process stream flow lines as shown in Figures 1 to 6. Where branches in the process stream occur (for example at the separation of oil and stickwater for the fish meal plant) the balance calculation follows one of the streams to completeness and returns to the branch point to pick up the remaining stream.

4) *Cost of Facilities and Site Development.*—This table summarizes the cost of land, docks, warehouses, and process buildings. The cost breakdown is similar to that described for Table 2. The data used in the calculations are stored in subroutine LIBRE and are printed out for easy reference in the table.

5) *Summary of Fixed Costs.*—This is a summation of total capital costs. It includes

the already detailed costs for equipment and facilities plus provisions for spare parts, engineering of the plant, and contingencies. The latter three are calculated as fractions of the summarized equipment cost.

6) *Operating Costs.*—This table presents the total and detailed plant operating costs on a daily and yearly basis. The quantities of all the materials used in the process and their daily costs are printed out first. This portion of the table contains also such items as electricity, packaging, and labor and supervision man-hours. Under the title "City Water" only the water used in the process which must be of drinking quality is included. The cost of process water (i.e. for scrubbers and condensers) is calculated in terms of the electricity needed to pump it.

The second portion of the table includes items which are calculated as fractions of the total capital or equipment costs. These are depreciation (at a percentage figure given in the input), maintenance, and insurance. The factors used to calculate these costs appear in subroutine OPERAT. Where not supplied in the input, the prices of the process material are stored under the designation BB(I) in subroutine LIBRE.

The third portion of the table summarizes the production rate of various products on a daily and yearly basis.

7) *Production Cost of FPC.*—The last table is entitled "Production Cost of FPC." In this table the following are listed:

- a) by-products of the process
- b) the assumed selling price in cents/pound
- c) the by-products total worth.

Two prices of FPC appear at the end of the printout. The first price is calculated by dividing total operating cost by the FPC produced per year. The second price takes into account the process by-products by subtracting their total worth from the total operating cost before dividing by the FPC produced per year. The calculations and printout take place in the subprogram OPERAT. The assumed selling prices of the by-products are found in LIBRE [BB(66) to BB(68)] and can easily be changed.

APPENDIX

A. Internal Program Changes

A-1. INTERNAL DATA CHANGES

There are several occasions when it may be necessary to update the program. These include the following:

- 1) The estimated cost of an item of equipment is in error
- 2) a new piece of equipment is to be added
- 3) the equipment sizing routine is to be altered
- 4) a new option is to be added to the plant options
- 5) a change in the cost of chemicals.

Most changes, especially of the types 1 and 5, may be made directly in the program LIBRE. Changes in bare cost, incidentals, labor, and materials for the process equipment may be made by substitution of the appropriate cards in LIBRE.

Example 1

The cards in LIBRE for a Rotary Dryer are:

AA (21,7) = 1000.
AA (21,8) = .5
AA (21,11) = .30
AA (21,12) = .30
AA (21,14) = .30

For these values the base cost of a dryer with 400 square feet is estimated to be \$20,000.

The manufacturer's estimates for this equipment were \$30,000, with the installed cost, labor cost, and incidentals estimated correctly.

Solution:

The base cost of the equipment too low. The simplest adjustment is to alter the base cost AA (21,7) to give the correct value. However, an increase of the base cost results in a incidental increase as well. The recommended solution is to substitute for the above cards in LIBRE the new cards.

AA (21,7) = 1500.
AA (21,8) = .50
AA (21,11) = .20
AA (21,12) = .20
AA (21,14) = .20

Example 2

The price of sulfuric acid is 30% more expensive at Plant A than it is at the other plants.

Solution:

The card [AA (100,14) = 1.00] in LIBRE is replaced with AA (100,14) = 1.30.

Occasionally in some items of equipment, such as a screw conveyor, one cannot alter the program by a single change of cards in LIBRE. The reason for this is that the base cost is a function of the diameter of the conveyor, which is an additional input variable to the costing subroutine. In this case it is necessary to alter the costing subroutine itself.

Example 3

The cost of the screw conveyor with a diameter greater than 2" has been found to overestimate the cost by a factor of 12. The labor cost, the incidentals, and the installation costs are correctly estimated. All other estimates are correct.

Here one cannot simply change LIBRE since the modification would appear for other sizes as well. There are many ways of modifying the program; one way would be to add the card to the subroutine SCREWWR.

If (AA (IX,18).GT.12.) AA (IX,7) = .5* AA (IX,7) which states that if the diameter is greater than 12 then the base cost is reduced by 50%.

The addition of a new equipment item requires three changes to the program.

1) First the new subroutine is named and given a previously unassigned index number. The Fortran statement of the program would be closely modeled after existing subroutines. It is strongly recommended that AA (IX,17) be used to designate the principal variable in the costing equation.

2) The variables for the costing equations are added to LIBRE. These should include

AA (IX,7)	Base Cost
AA (IX,8)	EXPONENT
AA (IX,11)	Materials
AA (IX,12)	Labor
AA (IX,13)	Incidentals
AA (IX,15)	Range of COSTS

3) The calling subroutine must be added to the primary subroutines. This calling sequence will include at least a sizing equation and the call statement.

```
AA (IX,17) = SIZE * .01/24  
CALL EQUIPM
```

A-2. EQUIPMENT SIZING AND PROCESS CHANGES

The equipment sizing routine is altered by changing statements in the primary subroutines.

Example 4

The area of heat exchangers in square feet was found to be 12% of the water evaporated rather than 10%, for the preheater to the distillation column.

Solution:

The subprogram XXIPA has the statement

```
FF = STEAMS * .1  
AA (67,17) = FF
```

These two cards are removed and replaced with

```
AA (67,17) = STEAMS * .12
```

Which not only makes the desired change but increases the efficiency of the program as well.

Major changes in program options must be made in the subprograms. In addition changes must be made in the main program as well. In general, there is no simple way of making these modifications.

Example 5

It is wished to add a costing subprogram for the VIOPIN program.

The procedure is to write a subprogram in Fortran for the VIOPIN program analogous to the program for the IPA process.

In addition changes are required in the program MAIN and the program OPERAT.

The user by referring to the above programs and using the example of the IPA process, can by analogy make the appropriate changes necessary for VIOPIN.

The printout can be modified by substitution of Format cards in the appropriate program.

B. References

1. Gaden, E. L., Jr., "World Protein Resources," Chem. Engr. Progress, 65, (9), September, 1969.
2. Roels, O. A., "Marine Protein," Chem. Engr. Progress, 65, (9), 27, September, 1969.
3. Klumpar, I. V., "Process Predesign by Computer," Chem. Engr., 76, 114, September 22, 1969.
4. Drayer, D. E., "How to Computerize Plant Cost Estimations," Petro/Chem. Engineer, 42, 39, May, 1970.
5. "Economic Indicators," Chem. Engr., 77, 250, May 4, 1970.
6. Guthrie, K. M., "Capital Cost Estimating," Chem. Engr., 76, 115, March 24, 1969.
7. Drew, J. W., and Ginder, A. F., "How to Estimate the Cost of Pilot-Plant Equipment," Chem. Engr., 77, 100, February 9, 1970.
8. Dryden, C. E., and Furlow, R. H., "Chemical Engineering Costs," Ohio State University, Columbus, 1966.
9. Mills, H. E., "Costs of Process Equipment," Chem. Engr., 71, 133, March 16, 1964.
10. Clerk, Jackson, "Multiplying Factors Give Installed Costs of Process Equipment," Chem. Engr., 70, 182, February 18, 1962.
11. Miller, C. A., "New Cost Factors," Chem. Engr., 72, 226, September 13, 1965.
12. "Centrifuges Exemplify Chem. Show Trends," Chem. & Engr. News, 56, December 15, 1969.
13. Ambler, C. M., "How to Select the Optimum Centrifuge," Chem. Engr., 76, 96, October 20, 1969.
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15. Drayer, D. E., "How to Estimate Plant Cost-Capacity Relationship," Petro/Chem. Engineer, 42, 10, May, 1970.
16. Kapfer, W. H., "Appraising Rate of Return Methods," Chem. Engr., Progress, 65, 55, November, 1969.
17. Ernst, R. C., "FPC: The NMFS Experiment and Demonstration Plant Process," Commercial Fisheries Review, 33(2), 22-28, February, 1971.

C. FORTRAN Listing of Program

The FORTRAN listing of the program appears as Table I.

D. Sample Problems

To illustrate the capabilities of the program a cost study spanning the feasible range of plant sizes was conducted. The plant capacities chosen were 50, 200, and 1,000 tons of fish per day. Fish availability time in each case was 200 days per year. For all processes except the Press cake-IPA this corresponds also to the plant operation time. For the Press cake-IPA process the IPA extraction portion of the plant

can operate for an additional 50 days to process the stored press cake. Fish food composition corresponded to a "lean" species (oil fraction = 0.04) and a "fat" species (oil fraction = 0.12). The price of fish was taken as 1¢/lb. for these examples.

1. SAMPLE OUTPUT

The entire output printout for an IPA process plant having a capacity of 200 tons/day and sized for a "lean" fish feed is presented in the subsequent pages. The number headings identifying the tables are explained in Section IV-E. The detailed equipment printout table, IPA Plant Cost Analysis, (Table II,) can be interpreted by following the process description given in Section III-C.

E. Study Summarization

The output of the study is summarized in Tables III to VI. The first three present data for each of the three plant capacities producing FPC. Table VI summarizes the results of the bench mark fish meal process.

349. Use of abstracts and summaries as communication devices in technical articles. By F. Bruce Sanford. February 1971, iii + 11 pp., 1 fig.

350. Research in fiscal year 1969 at the Bureau of Commercial Fisheries Biological Laboratory, Beaufort, N.C. By the Laboratory staff. November 1970, ii + 49 pp., 21 figs., 17 tables.

351. Bureau of Commercial Fisheries Exploratory Fishing and Gear Research Base, Pascagoula, Mississippi, July 1, 1967 to June 30, 1969. By Harvey R. Bullis, Jr., and John R. Thompson. November 1970. iv + 29 pp., 29 figs., 1 table.

352. Upstream passage of anadromous fish through navigation locks and use of the stream for spawning and nursery habitat, Cape Fear River, N.C., 1962-66. By Paul R. Nichols and Darrell E. Louder. October 1970, iv + 12 pp., 9 figs., 4 tables.

354. Sanitation guidelines for the control of *Salmonella* in the production of fish meal. By E. Spencer Garrett and Richard Hamilton. October 1971, iv + 7 pp., 9 figs. For sale by the Superintendent of Documents, U.S. Government Printing Office, Washington, D.C., 20402. Price 25 cents. Stock number 0320-0023.

356. Floating laboratory for study of aquatic organisms and their environment. By George R. Snyder, Theodore H. Blahm, and Robert J. McConnell. May 1971, iii + 16 pp., 11 figs.

361. Regional and other related aspects of shellfish consumption — some preliminary findings from the 1969 Consumer Panel Survey. By Morton M. Miller and Darrel A. Nash. June 1971, iv + 18 pp., 19 figs., 3 tables, 10 apps.

Table I.—FORTRAN listing of program.

FOR,S MAIN,MAIN
FOR 59A-07/12-11:03 (0,)

MAIN PROGRAM

STORAGE USED: CODE(1) 000407; DATA(0) 000330; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016
0005 BLOCK4 000012

EXTERNAL REFERENCES (BLOCK, NAME)

0006 LIBRE
0007 FPCXX1
0010 XXIPA
0011 BIOLOG
0012 PRESCK
0013 PRSIPA
0014 FASCIL
0015 CAPTOL
0016 OPERAT
0017 NINTR\$
0020 NRDU\$
0021 NIOP\$
0022 NRDC\$
0023 NPRT\$
0024 NSTOP\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	00010	100F	0000	000052	1001F	0000	000072	1002F	0000	000102	1003F
0000	00041	1007F	0000	000011	1011F	0000	000120	1011F	0000	000132	1012F
0000	00042	1013F	0000	000154	1014F	0000	000201	1016F	0000	000213	1017F
0000	00013	102F	0000	000226	1020F	0000	000244	1022F	0000	000255	1023F
0000	00015	103F	0000	000264	1030F	0000	000277	1032F	0000	000305	1033F
0000	000313	1034F	0000	000017	1040F	0000	000030	1041F	0001	000002	2L
0001	000304	200L	0001	000403	999L	0003	R	004704	BB	000000	COST
0004	R	000007	COSTA	0003	003720	IA	0005	I	000000	IPTION	IY
0000	I	000004	IW	0000	I	000003	IX	0000	I	000002	IY
0000	R	000007	TONS								

00100 1* C FPC PROCESS COST ANALYSIS PROGRAM
00101 2* COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
00103 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00104 4* COMMON/BLOCK4/ IPTION(10)
00105 5* DO 1 J = 1,7
00110 6* COST(J) = 0.0
00111 7* COSTA(J) = 0.0

Table I.--Continued.

```

00113      8*      CALL LIBRE
00114      9*      READ(5,100,END=999) IZ,IY,IX,IW,IV,IU
00124     100     FORMAT(8I10)
00125     11*     READ 101,TONS,RR(1),RR(50)
00132     12*     FORMAT(3E12.5)
00133     13*     BB(1) = BB(1)*297./280.
00134     14*     READ 102,RR(5),RR(6),RR(7),BB(8),BR(10)
00143     15*     FORMAT(5E12.5)
00144     16*     READ 103,RR(30),BR(31),BR(32)
00151     17*     FORMAT(3E12.5)
00152     18*     BB(91) = IZ
00153     19*     IPTION(1)=IY
00154     20*     IF(IZ.EQ.7) IPTION(5)=IW
00156     21*     FORMAT(//44H THE WET DEBONING OPTION IS APPROPRIATE)
00157     22*     FORMAT(//44H THE DRY DEBONING OPTION IS APPROPRIATE)
00160     23*     IF(IZ.EQ. 1) PRINT 1000
00163     24*     IF(IZ.EQ. 2) PRINT 1002
00166     25*     IF(IZ.EQ. 3) PRINT 1001
00171     26*     IF(IZ.EQ. 4) PRINT 1003
00174     27*     IF(IZ.EQ.7) PRINT 1007
00177     28*     FORMAT(1H1//20X,40H PRESS CAKE IPA PROCESS COST ANALYSIS )
00200     29*     FORMAT(1H1//20X,30H FISH MFAL PLANT COST ANALYSIS )
00201     30*     FORMAT(1H1//20X,30H TPA PLANT COST ANALYSIS )
00202     31*     FORMAT(1H1//20X,35H BIOLOGICAL PROCESS COST ANALYSIS )
00203     32*     FORMAT(1H1//20X,44H PRESS CAKE BIOLOGICAL PROCESS COST ANALYSIS )
00204     33*     PRINT 1010
00206     34*     FORMAT(//16H INPUT DATA )
00207     35*     PRINT 1011,TONS
00212     36*     PRINT 1012,RR(1)
00215     37*     PRINT 1013,RR(5)
00220     38*     PRINT 1014,RR(6)
00223     39*     PRINT 1017,RR(10)
00226     40*     PRINT 1015,RR(7)
00231     41*     PRINT 1016,RR(8)
00234     42*     PRINT 1030
00236     43*     BB(33)=100.0-BB(30)-BB(31)-BB(32)
00237     44*     PRINT 1031,RR(30)
00242     45*     PRINT 1032,RR(31)
00245     46*     PRINT 1033,RR(32)
00250     47*     PRINT 1034,RR(33)
00253     48*     FORMAT(//8X,11H PLANT SIZE )
00254     49*     FORMAT(//8X,31H MARSHAL/STEVENS INDEX )
00255     50*     FORMAT(//8X,31H COST OF FISH )
00256     51*     FORMAT(//8X,31H ELECTRICITY COSTS )
00257     52*     FORMAT(//8X,31H LABOR AND SUPV. COSTS )
00257     53*     )
00260     54*     1016 FORMAT(//8X,31H DEPRECIATION AND INT. CHARGE )
00261     55*     1017 FORMAT(//8X,31H FUEL COST )
00261     56*     CERM )
00262     57*     PRINT 1020
00264     58*     PRINT 1023,RR(50)
00267     59*     IF(IZ.NE.1) GO TO 200
00271     60*     IF(IY.EQ. 1) PRINT 1022
00274     61*     IF(IY.EQ. 2) PRINT 1021
00277     62*     200 CONTINUE
00300     63*     1020 FORMAT(//23H OPERATING OPTIONS )
00301     64*     1021 FORMAT(//8X,45H SOLURLE FISH SOLIDS RECYCLED TO MIXER IY=2 )

```


Table I.--Continued.

00302	65*	1022	FORMAT(/8X45H SOLUPLF FISH SOLIDS REMOVED AS PRODUCT TY=1)
00303	66*	1023	FORMAT(/8X26H OPERATING DAYS PER YEAR =,F8.0)
00304	67*	1030	FORMAT(/78X18H FISH COMPOSITION)
00305	68*	1031	FORMAT(/13X11H OIL =,F6.2,8H PERCENT)
00306	69*	1032	FORMAT(/13X11H PROTEIN =,F6.2,8H)
00307	70*	1033	FORMAT(/13X11H ASH =,F6.2,8H)
00310	71*	1034	FORMAT(/13X11H WATER =,F6.2,8H)
00311	72*		PTION(5)=IV
00312	73*		IF(IX.EQ.1) PRINT 1040
00315	74*		IF(IX.EQ.2) PRINT 1041
00320	75*		IF(IZ.EQ. 1) CALL FPCXX1(TONS)
00322	76*		IF(IZ.EQ.2) CALL YX1PA(TONS)
00324	77*		IF(IZ.EQ. 3) CALL RILOG(TONS)
00326	78*		IF(IZ.EQ. 4) CALL PRESCK(TONS)
00330	79*		IF(IZ.EQ.7) CALL PRSIPA(TONS)
00332	80*		CALL FASCIL(TONS)
00333	81*		CALL CAPTOL(TONS)
00334	82*		CALL OPERAT(TONS)
00335	83*	999	GO TO 2
00336	84*		STOP
00337	85*		END

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S FPCXX1,FPCXX1
FOR S9A-07/12-11:03 (0,)

SUBROUTINE FPCXX1 ENTRY POINT 002231

STORAGE USED: CODE(1) 002315; DATA(0) 000600; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK4 000012
0004 RLOCK1 005050
0005 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0006 PMPREC
0007 RELI
0010 STORAG
0011 PMPCNT
0012 BUCKET
0013 DRYERR
0014 SCREW
0015 SCREFN
0016 BLENDR
0017 HAMNER
0020 SCALE
0021 BAGGMA
0022 CNIFGE
0023 SHARP
0024 EVPHOR
0025 ROILER
0026 CONDEN
0027 WATER
0030 NPRT\$
0031 NI02\$
0032 NI01\$
0033 NEXP6\$
0034 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000214	1610F	0000	000005	1021F	0000	000047	1022F	0000	000203	1034F	0000	000174	1041F
0000	000215	1660F	0000	000226	1061F	0000	000237	1062F	0000	000250	1063F	0000	000261	1064F
0000	000272	1665F	0000	000303	1066F	0000	000314	1067F	0000	000325	1068F	0000	000336	1069F
0000	000347	1670F	0000	000360	1071F	0000	000371	1072F	0000	000413	1073F	0000	000402	1074F
0001	000027	111G	0001	000111	136G	0001	000146	155G	0000	000220	176G	0000	000103	2000F
0001	000377	250G	0001	000514	3L	0000	000116	3000F	0001	000602	327G	0001	000530	4L
0001	001032	422G	0000	000156	4242F	0001	001073	437G	0001	001457	51L	0001	000563	52L
0001	001663	664G	0004	000000	AA	0004	R 004704	BB	0000	R 000024	BULK	0005	R 000000	COST
0005	R 000007	COSTA	0000	R 000046	FISH	0000	R 000013	G	0000	R 000032	GAL	0000	R 000031	GALL
0000	R 000007	GALLON	0000	R 000010	GALS	0000	R 000014	HP	0000	R 000016	HPower	0000	I 000000	I
0004	I 003720	IA	0000	000557	INJPS	0003	I 000000	TPTTON	0000	I 000041	IXX	0000	I 000040	J
0000	I 000021	NA	0000	T 000023	NB	0000	I 000012	NUM	0000	I 000026	N1	0000	R 000042	PXX

Table I.-- Continued.

0000 R	000044	SCRUB	0000 R	000043	SOL	0000 R	000045	STM	0000 R	000011	SUMHP	0000 R	000015	TANK
0000 R	000033	TONA	0000 R	000034	TONB	0000 R	000035	TONC	0000 R	000037	TOND	0000 R	000006	TONSA
0000 R	000020	TONSB	0000 R	000022	TONSS	0000 R	000030	TONSSW	0000 R	000025	TONST	0000 R	000036	XLOOPS
0000 R	000017	XNUM	0000 R	000021	Z1	0000 R	000003	Z2	0000 R	000004	Z3	0000 R	000005	Z4
0000 R	000001	Z6	0000 R	000027	Z7									
00101	1*		SUBROUTINE FPCXX1(TONS)											
00101	2*	C	FISH MEAL PRODUCTION											
00101	3*	C												
00101	4*	C												
00103	5*		COMMON/BLOCK4/ IPTON(10)											
00104	6*		COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)											
00105	7*		COMMON/BLOCK2/ COST(7),COSTA(7)											
00106	8*		BB(3)=1.											
00107	9*		BB(2)=1.											
00110	10*		DO 10 I=30,33											
00111	11*		BB(I) = BB(I)*0.01											
00115	12*		BB(33) = 1.-BB(30)-BB(31)-BB(32)											
00116	13*		AA(91,2) = (BB(31)*.R5) + BB(32))* TONS*2.											
00117	14*		AA(91,3) = (1.2*TONS)-AA(91,2)											
00120	15*		Z6 = TONS*(BR(31)*.15)/AA(91,3)											
00121	16*		Z1=AA(91,3)/TONS											
00122	17*		Z2=AA(91,2)*.5/AA(91,3)											
00123	18*		Z3=TONS * BR(30)/(AA(91,3)+(.5*AA(91,2)))											
00124	19*		Z4=AA(91,2)/TONS											
00125	20*		1022 FORMAT(/ 25H PAYLOADER AND FORK LIFT , 10X ,15H											
00125	21*		1 , F10.3,30X,F10.3)											
00126	22*		1021 FORMAT(/ 25H CONTROL INSTRUMENTATION , 10X ,15H											
00126	23*		1 , F10.3,30X,F10.3)											
00127	24*		PRINT 2000											
00131	25*		2000 FORMAT(1H1//55H DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL											
00131	26*		CLARS))											
00132	27*		PRINT 3000											
00134	28*		3000 FORMAT (/18H EQUIPMENT TYPE,10X10H CAPACITY,12X0H MATERIAL,											
00134	29*		C60H BASE MATFRIALS LABOR INDIRECT MODULE RANGE ,/6											
00134	30*		C0X60H COST COSTS COSTS COSTS COST											
00135	31*		DO 1 I=1,7											
00140	32*		COSTA(I)=0.											
00141	33*		COST(I)=0.											
00142	34*		1 CONTINUE											
00142	35*	C	UNLOADING AND STORAGE OF FISH											
00142	36*	C												
00142	37*	C												
00144	38*		TONSA=TONS*2000./R*.33											
00145	39*		GALLON= TONSA/(24.*60.)											
00146	40*		GALS =GALLON*1.3											
00147	41*		SUMHP= 0.											
00150	42*		IA(65,1) = 0											
00151	43*		IA(65,2) = 1.0											
00152	44*		AA(65,17) = GALS*15											
00153	45*		NUM = TONS/600. +1											
00154	46*		DO 143 I=1,NUM											
00157	47*		SUMHP=SUMHP+(AA(65,17)*.001*1.5)											
00160	48*		143 CALL PMPREC											

Table I.-- Continued.

```

00162 49* IA(65,2) = 0.0
00163 50* IF (TONSA.LT.,30000.) G=(30000./(24.*60.))*15.
00165 51* IF (TONSA.GE.,30000.) G=(450000./(24.*60.))*15.
00167 52* IF (TONS.LE.,150.) AA(70,1A)= 3F.
00171 53* IF (TONS.GT.,150.) AA(70,1A)= 4A.
00173 54* AA(70,17)=100.
00174 55* CALL BELT
00175 56* DO 81 I=1,2
00200 57* AA(40,17)=TONS*32.05*3.
00201 58* IA(40,1)=0
00202 59* IA(40,2)=2
00203 60* CALL STORAG
00204 61* IA(40,2)=0
00205 62* CONTINUE
00207 63* AA(66,17)=30.*30.*TONS/(24.*60.)
00210 64* CALL PMPCNT
00211 65* HP=.001*AA(66,17)
00212 66* SUMHP=HP+SUMHP
00213 67* TANK=240.*TONS*1.
00214 68* IA(40,1)=2
00215 69* AA(40,17)=TANK
00216 70* AA(40,18)=1.0
00217 71* CALL STORAG
00220 72* TONSA=TONS*.8*2000./(8.33*16.)
00221 73* TONSA=TONSA*71/.8
00222 74* HPOWER=.01*TONSA
00223 75* NUM=(HPOWER/20.)*1.
00224 76* XNUMENJIM
00225 77* TONSB=TONS/24.
00226 78* AA(71,18)= TONSB
00227 79* AA(71,17)=20.
00230 80* CALL BUCKET
00230 81*
C FISH COOKERS AND SCRFW PRESS
00230 82* C
00230 83* C
00231 84* BB(2) = 0.67
00232 85* IA(21,5)= 2
00233 86* AA(21,17) = 0.25*TONS
00234 87* CALL DRYERR
00235 88* IA(21,5) = 0
00236 89* IF (TONS.GT.,300.) NA=(TONS/250.)*1.
00240 90* IF (TONS.LE.,300.) NA=(TONS/100.)*1.
C PUMP TO PRESS
00240 91* AA(66,17)=(AA(01,3)+AA(01,2))*2000.*30./(16.*60.**8.33)
00242 92* IA(66,1)=0
00243 93* CALL PMPCNT
00244 94* HP=.001*AA(66,17)
00246 96* SUMHP=SUMHP+HP
00247 97* DO 2 I= 1,NA
00252 98* IA(17,5)=3
00253 99* BB(2)=1.1
00254 100* IF (TONS.GT.,300.) AA(17,17) = 21.
00256 101* IF (TONS.GT.,300.) AA(17,18) = 16.
00260 102* IF (TONS.LE.,300.) AA(17,18) = 12.
00262 103* IF (TONS.LE.,300.) AA(17,17) = 15.
00264 104* CALL SCREW
00264 105* C PUMP FROM PRESS TO SCREEN

```

Table I.--Continued.

```

00265 106* AA(66,17)=AA(91,3)*2000.*30./(16.*60.*8.*33)
00266 107* IA(66,1)=0
00267 108* CALL PMPCNT
00270 109* HP=.001*AA(66,17)
00271 110* SUMHP=SUMHP+HP
00272 111* IF(TONS.GT.300.) AA(51,17)=5.0
00274 112* IF(TONS.LE.300.) AA(51,17)=2.0
00276 113* CALL SCREEN
00277 114* CONTINUE
00301 115* TONSS=TONS*74
00302 116* IF(IPTION(1),F0.2) TONSS=TONSS + (TONS*Z1*.26)
00304 117* IF(TONSS.GT.300.) GO TO 3
00306 118* NR=(TONSS/100.)+1
00307 119* AA(21,17)=100.*3.*R
00310 120* GO TO 4
00311 121* 3 NB=(TONSS/250.)+1
00312 122* AA(21,17)=250.*3.*R
00313 123* 4 CONTINUE
00313 124* C FISH MEAL STREAM
00313 125* C
00313 126* IF(IPTION(1),F0.1) GO TO 52
00314 127* FROM PRESS TO MIXER
00314 128* AA(66,17)=AA(91,2)*2000.*30./(16.*60.*8.*33)
00316 129* IA(66,1)=0
00317 130* CALL PMPCNT
00320 131* HP=.001*AA(66,17)
00321 132* SUMHP=SUMHP+HP
00322 133* AA(57,17)=(AA(91,2)+TONS*71*76*2.)*2000./62.4
00323 134* CALL BLENDR
00324 135* CONTINUE
00325 136* 52
00326 137* DO 5 I=1,NB
00331 138* IA(21,5)=3
00332 139* CALL DRYERR
00333 140* 5 CONTINUE
00333 141* C PUMP TO DRYER
00335 142* AA(66,17)=TONSS*2000.*30./(16.*60.*8.*33)
00336 143* IA(66,1)=0
00337 144* CALL PMPCNT
00340 145* HP=.001*AA(66,17)
00341 146* SUMHP=SUMHP+HP
00342 147* AA(91,18)=10.
00343 148* AA(81,17)=TONSS*0.33
00344 149* BULK=15.*TONS
00345 150* TONST=(TONS*Z4*.5)+(TONS*Z4*.5*Z3)
00346 151* AA(90,18)=TONS- TONST
00347 152* IF(IPTION(1),F0.2) AA(90,18)*2000./16.
00351 153* AA(90,18)=AA(90,18)*2000./16.
00352 154* IF(IPTION(1),F0.2) TONST= TONST + (TONS*Z1*76)
00354 155* AA(90,13)= TONS*74*.5*Z3*2000.*.01
00355 156* AA(57,17)=(AA(90,3)+AA(90,13)/2000.)*2000./62.4
00356 157* CALL BLENDR
00357 158* AA(90,3)=TONST
00357 159* FROM DRYER TO MIXER
00360 160* AA(66,17)=AA(90,3)*2000.*30./(16.*60.*8.*33)
00361 161* CALL PMPCNT
00362 162* HP=.001*AA(66,17)

```

Table I.-- Continued.

00363	163*	SUMHP=SUMHP+HP
00364	164*	AA(40,17)=(AA(00,3)+AA(90,13)/2000.)*2000./8.33*15.
00365	165*	IA(40,1)=0
00366	166*	CALL STORAG
00367	167*	CALL TO CURING
00368	168*	IA(66,1)=0
00370	169*	AA(66,17)=AA(40,17)*.30./(15.*16.*60.)
00371	170*	CALL PMPCNT
00372	171*	HP=.001*AA(66,17)
00373	172*	SUMHP=SUMHP+HP
00374	173*	AA(18,17)=1.30 * TONST/16.
00375	174*	CALL HAMMER
00376	175*	AA(72,17) = 1A.
00377	176*	CALL SCALE
00400	177*	IA(75,1)=0.0
00401	178*	IA(75,2)=0.0
00402	179*	AA(75,17)=AA(90,3)*20./ (60.*16.)
00403	180*	CALL BAGGMA
00404	181*	AA(75,17) = AA(75,17)*60*16
00405	182*	HP=XNUM*20.
00406	183*	SUMHP=SUMHP + (.001*HP)
00407	184*	AA(54,17)=Hp
00407	185*	C
00407	186*	FISH OIL STREAM
00407	187*	C
00410	188*	AA(40,17)=AA(91,3)*2000./ (16.*P.33)*1.
00411	189*	IA(40,1)=0
00412	190*	CALL STORAG
00413	191*	AA(66,17)=AA(40,17)*.30./60.
00414	192*	CALL PMPCNT
00415	193*	CALL PMPCNT
00416	194*	HP=.001*AA(66,17)
00417	195*	SUMHP=SUMHP+HP
00420	196*	SUMHP=SUMHP+HP
00421	197*	DO 11 I=1,N1M
00424	198*	AA(54,17)=20.
00425	199*	CALL CNTFGF
00427	200*	TONSA= TONSA Z3*1.1
00430	201*	HP=.025*TONSA
00431	202*	AA(52,17)= HP
00432	203*	N1=(HP/20.) +1.
00433	204*	HP=20*N1
00434	205*	SUMHP= SUMHP+ HP
00435	206*	AA(52,17)=20.
00436	207*	DO 12 I=1,N1
00441	208*	CALL SHARP
00443	209*	TONSA=TONS*.0*.8*.13*2000./8.33
00444	210*	TONSA=TONSA*Z1*Z3/(.8*.13)
00445	211*	Z7= 1.-Z3
00446	212*	IA(40,1)=2
00447	213*	AA(40,17)=TONSA*7./3.
00450	214*	AA(40,18)=1.0
00451	215*	CALL STORAG
00452	216*	IA(66,1)=0
00453	217*	AA(66,17)=TONSA*30./ (3.*16.*60.)
00454	218*	SUMHP= SUMHP +(AA(66,17)*.001)
00455	219*	SUMHP= SUMHP +(AA(66,17)*.001)

Table I.--Continued.

00456	220*	
00457	221*	AA(66,17)= AA(66,17)*30.
00460	222*	CALL PMPCNT
00460	223*	CALL PMPCNT
00460	224*	C FISH OIL STORAGE (15DAYS)
00460	225*	C
00461	226*	AA(90,5)=TONS*Z1*Z3
00462	227*	AA(40,17)=AA(90,5)*2000./A.33*15.
00463	228*	IA(40,1)=0
00464	229*	CALL STORAG
00465	230*	AA(66,17)=AA(40,17)*30./(60.*15.*16.)
00466	231*	CALL PMPCNT
00467	232*	HP=.001*AA(66,17)
00470	233*	SUMHP=SUMHP+HP
00470	234*	C FISH SOLUABLES STREAM
00470	235*	C
00470	236*	C PUMP TO ACID MIX TANK
00471	237*	TONSSW=TONS*71*Z7
00472	238*	IA(66,1)=0
00473	239*	AA(66,17)=30.*TONSSW*2000./(.8.*33*16.*60.)
00474	240*	CALL PMPCNT
00475	241*	HP=.001*AA(66,17)
00476	242*	SUMHP=SUMHP+HP
00477	243*	GALL=TONSSW*.2
00500	244*	GAL= TONSSW*.01
00501	245*	IA(40,1)=2
00502	246*	AA(40,17)= GAL*2000./(.8.*33)
00503	247*	AA(40,18)=1.0
00504	248*	CALL STORAG
00505	249*	IA(40,1)=2
00506	250*	AA(40,18)=1.0
00507	251*	AA(40,17)= GALL*2000./(.8.*33)
00510	252*	CALL STORAG
00511	253*	GAL=TONSSW*2000./(.8.*33*16.)
00512	254*	AA(66,17)=GAL*30./60.
00513	255*	SUMHP= SUMHP +(AA(66,17)*.001)
00514	256*	SUMHP= SUMHP +(AA(66,17)*.001)
00515	257*	IA(66,1) = 0
00516	258*	CALL PMPCNT
00517	259*	CALL PMPCNT
00520	260*	TONA=TONS*.87*.8*2000.*.001/(.8.*33* 1.82)
00521	261*	TONA=TONS*Z7*Z1/(.87*.8)
00522	262*	AA(90,14) = TONS*Z7*71*.001
00523	263*	AA(40,17)= TONA* 70.0
00524	264*	IA(40,1) = 1.0
00525	265*	IA(40,2) = 1.0
00526	266*	CALL STORAG
00527	267*	IA(40,1) = 0.0
00530	268*	IA(40,2) = 0.0
00531	269*	TONB= TONA/(16.*60.)
00532	270*	AA(66,17)= 30.*TONB
00533	271*	IA(66,1) = 2
00534	272*	CALL PMPCNT
00535	273*	SUMHP=SUMHP+(AA(66,17)*.001)
00536	274*	IA(66,1) = 0.0
00537	275*	TONA= TONS*.80*0.87* 2000./16.
00540	276*	TONA=TONA*Z1*77/(.8*.87)

Table I.--Continued.

```

00541 277* AA(33,17) = TONA / 20.
00542 278* CALL EVPHOR
00543 279* CALL EVPHOR
00544 280* CALL EVPHOR
00545 281* TONC = TONA*.06/(.87*.3)
00546 282* TONC=TONC*Z6*.87/(Z7*.06)
00547 283* C PUMP TO CONCENTRATOR
00548 284* AA(66,17)=TONC*20000.*30./(R.33*60.)
00549 285* IA(66,1)=0
00550 286* CALL PMPCNT
00551 287* HP=.001*AA(66,17)
00552 288* SUMHP=SUMHP+HP
00553 289* AA(33,17)=TONC/25.
00554 290* CALL EVPHOR
00555 291* AA(90,4)=TONS*Z1*Z6*.1.
00556 292* AA(40,17)=AA(90,4)*2000./(R.33*16.)*1.
00557 293* IA(40,1)=0
00558 294* CALL STORAG
00559 295* AA(66,17)=30.*AA(40,17)/60.
00560 296* CALL PMPCNT
00561 297* HP=.001*AA(66,17)
00562 298* SUMHP=SUMHP+HP
00563 299* SUMHP=SUMHP+HP
00564 300* IF(IPTION(1).EQ.2) GO TO 51
00565 301* C CONDENSED FISH SOLUBLES STORAGE (15 DAYS)
00566 302* C
00567 303* AA(40,17)=AA(90,4)*2000./R.33*15.
00568 304* IA(40,1)=0
00569 305* CALL STORAG
00570 306* C
00571 307* 51 CONTINUE
00572 308* C
00573 309* C SUMMATION OF STEAM, WATER, AND ELECTRICITY
00574 310* C
00575 311* AA(27,18)=150.
00576 312* AA(27,17)= TONS*2.*2000./(3.*16.)
00577 313* C BOILER WATER TREATMENT
00578 314* C
00579 315* COST(5)=1.000
00580 316* COST(1)=COST(5)
00581 317* PRINT 4242,COST(1),COST(5)
00582 318* 4242 FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H
00583 319* ,F10.3,30X,F10.3)
00584 320* COSTA(1)=COSTA(1)+COST(1)
00585 321* COSTA(5)=COSTA(5)+COST(5)
00586 322* C FUEL OIL STORAGE
00587 323* C
00588 324* IA(40,1)=2
00589 325* AA(40,17)=TONS*6000./387.*15.
00590 326* CALL STORAG
00591 327* AA(66,17)=30.*AA(40,17)/(15.*60.)
00592 328* CALL PMPCNT
00593 329* HP=.001*AA(66,17)
00594 330* SUMHP=SUMHP+HP
00595 331*
00596 332*
00597 333*

```


Table I.- Continued.

```

nn620 334*
nn621 335*
nn622 336*
nn623 337*
nn624 338*
nn625 339*
nn626 340*
nn626 341*
nn626 342*
nn626 343*
nn630 345*
nn631 346*
nn632 347*
nn633 348*
nn634 349*
nn635 350*
nn636 351*
nn637 352*
nn640 353*
nn641 354*
nn645 355*
nn646 356*
nn647 357*
nn650 358*
nn651 359*
nn652 360*
nn653 361*
nn657 362*
nn660 363*
nn661 364*
nn662 365*
nn670 366*
nn671 367*
nn672 368*
nn674 369*
nn675 370*
nn677 371*-
nn700 372*
nn701 373*
nn702 374*
nn703 375*
nn704 376*
nn705 377*
nn706 378*
nn707 379*
nn710 380*
nn711 381*
nn712 382*
nn712 383*
nn712 384*
nn712 385*
nn713 386*
nn714 387*
nn715 388*
nn716 389*
nn721 390*

CALL BOILER
XLOOPS= 9 + NA +NB
TOND=TONA/2.4 -TONC/2.4 +(TONC*.4)
AA(9,1,5) = (TONA-TOND)/(0.6*8.33)
AA(9,1,7) = (TONC*.4)
AA(9,1,6) = (TONA-TOND)/2.4
AA(66,17) = 4*(AA(9,1,6) +AA(9,1,7)) +1.5*TONS

C SEA WATER PUMPS
C
IA(66,1)=1
IA(66,4)=2
CALL PMPCNT
IA(66,1)=0
IA(66,4)=0
SUMHP= SUMHP +(AA(66,17)*.001*1.5)
COST(1)=XLOOPS *AA(100,1)
COST(5)=COST(1)
COSTA(1) = COSTA(1) + COST(1)
COSTA(5)=COSTA(5) + COST(5)
PRINT 1021 COST(1),COST(5)
AA(8,17) = TONS
CALL CONDEN
COST(1)=AA(100,2)
COST(5)=COST(1)
COSTA(1)=COST(1) + COSTA(1)
COSTA(5)=COSTA(5) + COST(5)
PRINT 1022, COST(1),COST(5)
AA(72,17)=1R.
CALL SCALE
CALL SCALE
PRINT 1041,(COSTA(J),J=1,6)
FORMAT(//25H TOTAL COSTS
1041 ,35X6F(0.3)
COSTA(7)=0.02*COSTA(1)
IF(IPTION(1),E0.2) AA(90,4)=0.
1034 FORMAT(// 40H TOTAL COST OF FEPC PLANT
PRINT 1010 ,F16.3)
FORMAT(1H1)
HP = TONS*.00124 +13.6
SUMHP = HP + SUMHP
HP = 40*TONS/3.
SUMHP = HP + SUMHP
AA(90,2)= SUMHP* .7457 * 16.
AA(100,10)=COSTA(5)
IXX =(16.0*(TONS/50.0)**.31) +0.5
PXX =IXX
AA(90,9) =PXX*10.
AA(90,8) =IXX*8.0

C MATERIAL BALANCE INFORMATION PRINTOUT
C
CALL MATER(TONS)
TONS = TONS/16
AA(90,15)= TONS*2000.*.2
PRINT 1060,AA(90,15)
FORMAT(/8X26H COOKERS STFAM
1060 ,F8.0,7H LB/HR )

```

Table I.--Continued.

00722	391*	AA(91,3)= AA(91,3)* 2000./16.	
00723	392*	AA(91,2)= AA(91,2)* 2000./16.	
00724	393*	PRINT 1061,AA(91,3)	
00727	394*	PRINT 1062,AA(91,2)	
00732	395*	FORMAT(/8X26H PRES LIQUOR	,F8.0,7H LB/HR)
00733	396*	FORMAT(/8X26H PRES CAKE	,F8.0,7H LB/HR)
00734	397*	AA(91,1)= AA(91,3)*.77	
00735	398*	PRINT 1063,AA(91,1)	
00740	399*	FORMAT(/8X26H STICK WATER	,F8.0,7H LB/HR)
00741	400*	AA(90,5) = AA(90,5)*2000.0/16	
00742	401*	PRINT 1064, AA(90,5)	
00745	402*	FORMAT(/8X26H FISH OIL	,F8.0,7H LB/HR)
00746	403*	PRINT 1065,AA(90,16)	
00751	404*	FORMAT(/8X26H TRIPLF EVAP. STFAM	,F8.0,7H LB/HR)
00752	405*	AA(91,4)= 0.15*BB(31)*.01*TONS*2000.0/0.30	
00753	406*	PRINT 1066 ,AA(91,4)	
00756	407*	FORMAT(/8X26H TRIPLF EVAP. CONCENTRATE	,F8.0,7H LB/HR)
00757	408*	AA(91,5)=AA(90,16)*4.0	
00760	409*	PRINT 1067 ,AA(91,5)	
00763	410*	FORMAT(/8X26H TRIPLF EVAP. COOLING	,F8.0,7H GAL/HR)
00764	411*	PRINT 1068,AA(90,17)	
00767	412*	FORMAT(/8X26H CONCENTRATOR EVAP. STEAM	,F8.0,7H LB/HR)
00770	413*	AA(91,6) =AA(90,17)*4.0	
00771	414*	PRINT 1069,AA(91,6)	
00774	415*	FORMAT(/8X26H CONC. COOLING WATER	,F8.0,7H GAL/HR)
00775	416*	SOL =AA(90,4)*2000.0/16	
00776	417*	PRINT 1070,SOL	
01001	418*	FORMAT(/8X26H FISH SOLUBILES	,F8.0,7H LB/HR)
01002	419*	AA(90,18)=AA(90,1A)/16	
01003	420*	PRINT 1071,AA(90,18)	
01006	421*	FORMAT(/8X26H DRYFR STEAM	,F8.0,7H LB/HR)
01007	422*	SCRUB=180*TONS	
01010	423*	PRINT 1072,SCRUB	
01013	424*	FORMAT(/8X26H SCRIBFR WATFR	,F8.0,7H GAL/HR)
01014	425*	STM=AA(27,17)-AA(90,18)-AA(90,17)-AA(90,16)	
01015	426*	PRINT 1074,STM	
01020	427*	FORMAT(/8X26H MISCEI ANEOUS STEAM	,F8.0,7H LB/HR)
01021	428*	FISH =AA(90,3)*2000.0/16	
01022	429*	PRINT 1073,FISH	
01025	430*	FORMAT(/8X26H FISH MFAL	,F8.0,7H LB/HR)
01026	431*	TONS = TONS*16	
01027	432*	AA(90,5) = AA(90,5)*16.0/2000.0	
01030	433*	AA(91,2)= AA(91,2)*16./2000.	
01031	434*	AA(91,3)= AA(91,3)*16./2000.	
01032	435*	AA(90,13) = AA(90,13) + (AA(90,3)+AA(90,7)+AA(90,20)+AA(90,4))	
01033	436*	AA(90,14)=AA(90,14)*2000.	
01034	437*	RETURN	
01035	438*	END	

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S PRSIPA, PRSIPA
FOR 59A-07/12-11:03 (1,)

SUBROUTINE PRSIPA ENTRY POINT 003537

STORAGE USED: CODE(1) 003617; DATA(0) 001410; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK2 000016
0004 DATA 000050
0005 RLOCK1 005050
0006 RLOCK4 000012

EXTERNAL REFERENCES (BLOCK, NAME)

0007 PMPREC
0010 BELT
0011 SCALE
0012 STORAG
0013 REFRIG
0014 SILO
0015 RUCKET
0016 DRYERR
0017 SCREWRR
0020 SCRFEN
0021 PMPCNT
0022 GRINDR
0023 REACTR
0024 AGITOR
0025 HEATEX
0026 COLUMN
0027 VESSEL
0030 CNTFGE
0031 SHARP
0032 EPHOR
0033 HAMNER
0034 BAGGMA
0035 HOILER
0036 CONDEN
0037 WATER
0040 SQRT
0041 NPRT\$
0042 NIO2\$
0043 NIO1\$
0044 NEXP6\$
0045 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000453	1003F	0000	000364	1021F	0000	000375	1022F	0000	000443	1041F	0001	000020	1136
0000	000464	1201F	0000	000476	1202F	0000	000510	1203F	0000	000522	1204F	0001	003005	1204G
0000	000534	1205F	0000	000546	1206F	0000	000560	1207F	0000	000572	1208F	0000	000617	1209F

Table I.--Continued.

0001	00025	121G	00054	1210F	000632	1211F	000644	1212F	000656	1213F
0000	00074	1214F	000705	1215F	000716	1216F	000727	1217F	000740	1218F
0000	000751	1219F	000762	1220F	000773	1221F	000784	1222F	000795	1223F
0000	001026	1224F	001040	1225F	001052	1226F	001064	1227F	001076	1228F
0000	001110	1230F	001122	1231F	001134	1232F	001146	1233F	000032	1276
0001	003210	1330G	003221	1336G	003232	1344G	003243	1352G	000032	1366
0001	003265	1366G	003276	1374G	003307	1402G	003320	1410G	003331	1416G
0001	000144	163G	000341	237G	000340	3000F	000352	3006F	000605	323G
0001	000671	345G	000702	350G	000734	361G	000735	364G	000755	372G
0001	000760	377G	000407	4242F	000425	4243F	001145	433G	002574	44L
0001	001226	450G	002574	49L	001336	507G	0012273	51L	001400	516G
0001	002417	52L	002137	716G	002206	734G	000000	AA	000240	ABC
0000	R 000245	ACID	R 004704	BB	R 000000	COST	R 000007	COSTA	R 000000	DATR
0000	R 000172	DAYS	R 000173	DAYSR	R 000273	DAZ0IL	R 000201	DENS	R 000216	DRYSLD
0000	R 000241	DX	R 000203	FACT10	R 000310	FISH	R 000211	G	R 000246	GAL
0000	R 000206	GALLON	R 000207	GALS	R 000272	H0TH20	R 000171	HOUR	R 000212	HP
0000	R 000276	HWAT	R 000167	I	R 000320	IA	R 0001346	INJP\$	R 000234	IP
0006	I 000000	IPTION	R 000230	IR	R 000231	rRR	R 000235	IU	R 000337	IXX
0000	I 000224	J	R 000325	K	R 000176	LOOPS	R 000166	MATRL	R 000214	NA
0000	I 000204	NOREAC	R 000225	NQUIP	R 000210	NUM	R 000223	NUMZ	R 000242	NUTH
0000	I 000302	NZ	R 000271	N2	R 000266	N3	R 000265	OIL	R 000262	PRDCTA
0000	R 000263	PRDCTB	R 000247	SAA	R 000267	SAB	R 000244	SACID	R 000233	SAG
0000	R 000300	SAQT	R 000161	SB0T	R 000255	SB0TT	R 000275	SB0GT	R 000274	SB0T
0000	R 000270	SCB	R 000175	SOLL10	R 000177	STEAM1	R 000256	STEAMR	R 000200	STEAMW
0000	R 000250	STEAM1	R 000251	STEAM2	R 000252	STEAM3	R 000253	STEAM4	R 000306	STEAM6
0000	R 000254	STEAM9	R 000000	STM	R 000143	STMM	R 000154	STOP	R 000055	STRM
0000	R 000132	STRMM	R 000170	SUMHP	R 000232	TANK	R 000257	TANKA	R 000301	TASA
0000	R 000303	TASB	R 000304	TASC	R 000305	TASD	R 000277	TONA	R 000205	TONSA
0000	R 000213	TONSG	R 000222	TONSX	R 000226	VES	R 000227	VESS	R 000261	WASTE
0000	R 000174	WATAD	R 000264	WATER	R 000202	WAT0IL	R 000260	WIDTH	R 000236	XIP
0000	R 000237	XIR	R 000243	XIRR	R 000217	XL10D	R 000307	XL00PS	R 000215	XNA
0000	R 000220	XOIL	R 000221	X50L	R 000326	XXA	R 000327	XXB	R 000330	XXC
0000	R 000331	XXD	R 000332	XXE	R 000333	XXG	R 000334	XXH	R 000335	XXI
0000	R 000336	XXJ	R 000311	YYA	R 000312	YYB	R 000313	YYC	R 000314	YYD
0000	R 000315	YYE	R 000316	YYG	R 000317	YYH	R 000320	YYI	R 000321	YYJ
0000	R 000322	YYK	R 000323	YYL	R 000324	YYM				

00101 1* SUBROUTINE PRSIP(ATIONS)
00103 2* COMMON/BLOCK2/ COST(7),COSTA(7)
00104 3* COMMON/ DATA1 / DATR(8,5)
00105 4* COMMON/BLOCK1/ AA(100,20),IA(100,5),BR(100)
00106 5* COMMON/BLOCK4/ IPTION(10)
00107 6* DIMENSION STM(5,9),STRM(5,9),STRMM(9),STMM(9)
00110 7* DIMENSION STOP(5),SB0T(5)
00111 8* REAL MATRI
00111 9* C
00111 10* C NORMALIZATION
00111 11* C
00112 12* DO 1 I=1,7
00115 13* COST(I) = 0.
00116 14* COSTA(I)= 0.
00120 15* DO 2 I=1,20
00123 16* AA(90,I)=0.
00124 17* AA(91,I)=0.
2

Table I.--Continued.

```

00126 18*
00131 19*
00133 20*
00134 21*
00135 22*
00136 23*
00137 24*
00140 25*
00141 26*
00141 27*
00142 28*
00143 29*
00144 30*
00145 31*
00146 32*
00147 33*
00150 34*
00151 35*
00151 36*
00151 37*
00151 38*
00153 39*
00154 40*
00155 41*
00156 42*
00157 43*
00160 44*
00161 45*
00162 46*
00165 47*
00166 48*
00170 49*
00171 50*
00173 51*
00175 52*
00177 53*
00201 54*
00202 55*
00203 56*
00204 57*
00205 58*
00206 59*
00207 60*
00210 61*
00211 62*
00213 63*
00214 64*
00214 65*
00215 66*
00216 67*
00217 68*
00220 69*
00221 70*
00222 71*
00223 72*
00224 73*
00225 74*

DO 10 I =30,33
BB(I)=BB(I)* 0.01
SUMHP= 0.
HOUR= 24.
DAYS= 30.
AA(72,17)=18.
DAYSR = 3.
WATAU = 0.2
SOLLIO= 2.5
LOOPS=0
STEAM=0.
STEAMW = 0.
DENS = 0.9
WATOIL=2.
FACT10=1.
NOREAC= IPTION(5)
IF(NOREAC.EQ.0) NORFAC = 4

C STEAMW IS THE STEAM REQUIRED FOR THE WET DEBONING OPTION

C UNLOADING AND STORAGE OF FISH
C
TONSA = TONS* 2000./R.33
GALLON= TONSA / (HOUR* 60.)
GALS = GALLON * 1.3
IA(65,1) = 0.
IA(65,2) = 1.0
AA(65,17)= GALS * 30.
NUM =(TONS/500.) + 1
DO 143 I=1,NUM
SUMHP= SUMHP +(2.*AA(65,17)*.0015)
CALL PMPREC
IA(65,2) = 0.
IF(TONSA.LT.30000.) G = 30000./(24.*60.) * 15.
IF(TONSA.GE.30000.) G = 450000./(24.*60.) * 15.
IF(TONS.LE.150.) AA(70,18) = 36.
IF(TONS.GT.150.) AA(70,18) = 48.
AA(70,17)= 100.
CALL BELT
CALL SCALE
HP=(TONS * 0.00124 ) + 13.6
SUMHP = HP + SUMHP
AA(40,17) = DAYS * TONS
IA(40,1) = 0.
IA(40,2) = 2
CALL STORAG
IA(40,2) = 0
AA(85,17) = 0.5* TONS * DAYSR
IA(85,1) = 30
SUMHP= SUMHP +(4.72*AA(85,17))
IA(7,1) = 1
AA(7,17) = 27.4* TONS
CALL SILO
TONSG = TONS/24.
AA(71,18) = TONSG
AA(71,17) = 20.
CALL BUCKET

```

Table I.--Continued.

00226	75*	HP= TONS * 0.00106	
00227	76*	SUMHP = HP + SUMHP	
00227	77*		
00227	78*	C FISH COOKERS AND SCREW PAFSS	
00227	79*	C	
00230	80*	AA(91,16) = WATAD* TONS	
00231	81*	AA(91,10) = TONS + AA(91,16)	
00232	82*	IF(TONS.GT.450) NA= (TONS/250.)+ 1.	
00234	83*	IF(TONS.LE.450) NA= (TONS/100.)+ 1.	
00236	84*	DO 3 I=1,NA	
00241	85*	BB(2)=2.1	
00242	86*	XNA=NA	
00243	87*	IA(21,5) = 4	
00244	88*	AA(21,17)= TONS/XNA	
00245	89*	CALL DRYERR	
00246	90*	IA(17,5) = 3	
00247	91*	BB(2)=2.6	
00250	92*	IF(TONS.GT.450.) AA(17,17)= 21.	
00252	93*	IF(TONS.GT.450.) AA(17,18)= 16.	
00254	94*	IF(TONS.LE.450.) AA(17,18)= 12.	
00256	95*	IF(TONS.LE.450.) AA(17,17)= 15.	
00260	96*	CALL SCREW	
00261	97*	IF(TONS.GT.450) AA(51,17)= 10.	
00263	98*	IF(TONS.LE.450) AA(51,17)= 4.	
00265	99*	CALL SCREEN	
00266	100*	3 CONTINUE	
00270	101*	DRYSLD=(BB(31)+0.45*BB(31))*TONS	
00271	102*	XLIQD= (BB(31)*0.15+ BB(30)+ BB(33))* TONS +AA(91,16)	
00272	103*	XOIL= BB(30) * TONS/XLIQD	
00273	104*	XSOL= BB(31) * 0.15* TONS/XLIQD	
00274	105*	AA(90,16)= DRYSLD * SOLLIQ	
00275	106*	AA(90,18)=AA(91,10)-AA(90,16)	
00275	107*	C SOLIDS STREAM - AA(90,16)	
00275	108*	C	
00275	109*	TONSX=TONS	
00276	110*	TONS=AA(90,16)*FACT10	
00277	111*	TONSG = AA(90,16) / HOUR	
00300	112*	AA(7,17) = 50.0* AA(90,16) / (62.4*DENS) * 2000.	
00301	113*	IA(7,1) = 1	
00302	114*	CALL SILO	
00303	115*	AA(66,17) = AA(90,16)*2000./(HOUR*8.33*60.) * 25.	
00304	116*	CALL PMPCNT	
00305	117*	HP= AA(66,17)/25.	
00306	118*	SUMHP = HP+ SUMHP	
00307	119*	CALL PMPCNT	
00310	120*	SUMHP= HP + SUMHP	
00311	121*	IF (TONSG .GT.6) AA(50,17)= 6.	
00312	122*	IF (TONSG .GT.6) NUMZ = (TONSG/6.) + 1.	
00314	123*	IF (TONSG .LE.6) AA(50,17)= 3.	
00320	125*	IF (TONSG .LE.6) NUMZ = (TONSG/3.) + 1.	
00322	126*	DO 720 J= 1,NUMZ	
00325	127*	720 CALL GRINDR	
00327	128*	HP= 40.* TONSG/3.	
00330	129*	SUMHP= HP + SUMHP	
00330	130*	C EXTRACTION VESSEI S MATERIAL BALANCE	
00330	131*	C	

Table I.-- Continued.

```

00330 C 1-OIL 2-PROTEIN 3-ACA 4-WATER 5-IPA NOREAC=NUMBER OF REACTORS
00330 C
00331 NQUIP= NOREAC + 1
00332 STM(1,1) = (SOLLIO-1.)*DRYSLD*XOIL
00333 STM(3,1)=DRYSLD*BR(32)/(HR(32) + (0.85*RB(31)))
00334 STM(2,1)=(DRYSLD-STM(3,1)) + ((SOLLIO-1.)*DRYSLD*XSOI)
00335 STM(4,1) = (SOLLIO-1.)*DRYSLD*(1.- XSOI-XOIL)
00336 STM(5,1) = 0.0
00337 STRM(1,NQUIP)=0.
00338 STRM(2,NQUIP)=0.
00339 STRM(3,NQUIP)=0.
00340 STRM(4,NQUIP) = WATNLI*2.804*AA(90,16)/22.264
00341 STRM(5,NQUIP) = STRM(4,NQUIP)*19.46/2.804
00342 DO 121 I=1,NOREAC
00343 DO 121 J=1,5
00344 STM(J,I+1) = STM(J,I)*DATH(I,J)
00345 IF(I.EQ.1.AND.J.EQ.5) STM(5,2) = STM(4,1)*DATH(1,5)
00346 121 CONTINUE
00347 DO 122 I=NORFAC,1,-1
00348 DO 122 J=1,5
00349 STRM(J,I) = STRM(J,I+1) - STM(J,I+1)*STM(J,I)
00350 DO 123 I=1,NQUIP
00351 STRMM(I)=0.
00352 STRMM(1)=0.
00353 DO 123 J=1,5
00354 STRMM(I) = STRMM(I) + STM(J,I)
00355 123 CONTINUE
00356 C REACTOR VESSELS
00357 C
00358 VES= TONS* 30.
00359 AA(49,17) = VES
00360 VESS = TONS* 16.
00361 IR= 1
00362 IF(VES.GT.10000.) IR= (VES/10000.) + 1.
00363 IF(VES.GT.10000.) VFS = 10000.
00364 IRR=1
00365 IF(VESS.GT.10000.) IRR=(VESS/10000.) + 1.
00366 TANK = 800.* TONS / 50.
00367 AA(40,18)=3.2
00368 AA(41,18)=3.2
00369 AA(40,17)= TANK
00370 CALL STORAG
00371 SAG= STRMM(2) * 2000./(24.*8.33*60.) *(24./HOUR)
00372 IP=1
00373 IF(SAG.GT.12500.) TP=(SAG/12500.) + 1.
00374 DO 93 IU=1,TP
00375 XIP=IP
00376 AA(66,17) =(SAG/XIP) * 24.
00377 CALL PMPCNT
00378 CONTINUE
00379 93 MISCELLA TANK
00380 IF ( VESS.GT.10000.) VFS= 10000.
00381 XIP=IR
00382 IP=(TONS*60./(50.*144.*XIP)) + 2.
00383 AA(51,17) = IP
00384 186*
00385 187*
00386 188*
00387 189*
00388 190*
00389 191*
00390 192*
00391 193*
00392 194*
00393 195*
00394 196*
00395 197*
00396 198*
00397 199*
00398 200*
00399 201*
00400 202*
00401 203*
00402 204*
00403 205*
00404 206*
00405 207*
00406 208*
00407 209*
00408 210*
00409 211*
00410 212*
00411 213*
00412 214*
00413 215*
00414 216*
00415 217*
00416 218*
00417 219*
00418 220*
00419 221*
00420 222*
00421 223*
00422 224*
00423 225*
00424 226*
00425 227*
00426 228*
00427 229*
00428 230*
00429 231*
00430 232*
00431 233*
00432 234*
00433 235*
00434 236*
00435 237*
00436 238*
00437 239*
00438 240*
00439 241*
00440 242*
00441 243*
00442 244*
00443 245*
00444 246*
00445 247*
00446 248*

```

Table I.-- Continued.

```

00447 189*
00452 190*
00453 191*
00454 192*
00455 193*
00456 194*
00457 195*
00461 196*
00462 197*
00463 198*
00464 199*
00465 200*
00466 201*
00467 202*
00470 203*
00471 204*
00473 205*
00475 206*
00476 207*
00477 208*
00500 209*
00501 210*
00502 211*
00503 212*
00505 213*
00505 214*
00505 215*
00505 216*
00506 217*
00511 218*
00512 219*
00513 220*
00514 221*
00515 222*
00520 223*
00521 224*
00522 225*
00523 226*
00524 227*
00525 228*
00527 229*
00531 230*
00532 231*
00533 232*
00534 233*
00535 234*
00536 235*
00540 236*
00541 237*
00542 238*
00543 239*
00544 240*
00545 241*
00546 242*
00547 243*
00550 244*
00553 245*

DO 41 I =1,TR
LOOPS= LOOPS + 3
AA(49,17) = VFS
CALL REACTR
CALL SCREEN
AA(73,17) = 0.005* VFS
IF(AA(73,17).LT.2.) AA(73,17)=2.
IA(73,5) = 2.
CALL AGITR
SUMHP = SUMHP + 2.5
XIR=IR
SUMHP= SUMHP+ AA(73,17)
AA(66,17)= TONS* 2000./(HOUR*.8.33*XIR) * (22./60.)
CALL PMPCNT
ABC= AA(66,17)/22.
IF(ABC.LE.2.) HP= 2.
IF(ABC.GT.2.) HP= ABC
SUMHP= HP + SUMHP
IA(17,5) = 5
DX= SQRT(TONS/50.) * 8. /SQRT(XIP)
AA(17,17) = 6
AA(17,18) = DX
CALL SCREW
41 CONTINUE
NUTHENOREAC = 1
C
C OTHER REACTION VFSSELS
C
DO 42 J = 1,IRR
XIP=IRR
IP=(TONS*60./(50.*XIP*144.)) + 2.
AA(51,17)=IP
LOOPS= LOOPS + (3*NUTH)
DO 42 I = 1,3
XIRR=IRR
SUMHP=SUMHP + 2.5
AA(66,17)= TONS*2000./(24.*8.33*XIRR)*(22./60.)
CALL PMPCNT
ABC= AA(66,17)/ 22.
IF(ABC.GT.2.) HP=ABC
IF(ABC.LE.2.) HP=2.
SUMHP= SUMHP + HP
AA(49,17)= VESS
CALL REACTR
CALL SCREEN
AA(73,17)= 0.005*VESS
IF(AA(73,17).LT.2.) AA(73,17)= 2.
IA(73,5) = 2
SUMHP = SUMHP + AA(73,17)
CALL AGITR
DX= SQRT(TONS/50) * 8. / SQRT(XIP)
AA(17,18)= DX
AA(17,17)= 6.
IA(17,5)= 5
CALL SCREW
42 CONTINUE
TONS=TONSX

```


Table I.--Continued.

```

00553 246* C
00553 247* C MIXING TANK SECTION
00553 248* C
00554 249* SACID= STRMM(1)*.001*70.
00555 250** IA(40,1)= 1
00556 251* IA(40,2)= 1
00557 252* AA(40,17) = SACID
00560 253* CALL STORAG
00561 254* ACID STORAGE TANK
00561 255* IA(40,2) = 0
00562 256* LOOPS=LOOPS+ 2
00563 257* ACID = STRMM(1) *.001
00564 258* IA(66,1) = 2
00565 259* AA(66,17)= 30.*ACID* 2000./ (A.33*60.*HOUR*1.8)
00566 260* CALL PMPCNT
00566 261* FROM ACID STORAGE TO MIX TANK
00567 262* GAL=STRMM(1)* 2000./ (8.33 )
00570 263* SUMHP= SUMHP + (.0015*AA(66,17) )
00571 264* AA(40,17) = GAL *.01
00572 265* AA(66,17) = GAL *40./ (HOUR*60.)
00573 266* IA(66,1) = 0
00574 267* IA(40,1) = 2
00575 268* SUMHP= SUMHP + (AA(66,17)*.0015)
00576 269* CALL PMPCNT
00577 270* FROM PRESS TO ACID MIX TANK
00577 271* CALL STORAG
00577 272* ACID MIX TANK
00600 273* CALL PMPCNT
00600 274* FROM ACID MIX TANK TO MISCELLA TANK
00600 275* C
00600 276* C MISCELLA TANK BEFORE PREHEATER ( 1 HOUR HOLDUP)
00600 277* C
00601 278* SAA= 1.001* STRMM(1)
00602 279* AA(40,17)= SAA*2000./ (HOUR*8.33)
00603 280* IA(40,1) = 1
00604 281* CALL STORAG
00605 282* AA(66,17) = 30. * AA(40,17)
00606 283* IA(66,1) = 0
00607 284* CALL PMPCNT
00610 285* SUMHP = SUMHP + (.0015*AA(66,17) )
00611 286* PRINT 3000
00613 287* 3000 FORMAT(/50H STORAGE TANK BEFORE PREHEATER
00613 288* C
00613 289* C STEAM REQUIREMENTS
00613 290* C
00614 291* STEAM1 = AA(90,16)*FACTIN*35./50.
00615 292* STEAM2 = AA(90,16)*FACTIN*20./50.
00616 293* STEAM3 = AA(90,16)*FACTIN*20./50.
00617 294* STEAM4 = AA(90,16)*FACTIN*20./50.
00620 295* STEAM = STEAM1+STFAM2+STFAM3+STEAM4
00620 296* PREHEATER FOR DISTILLATION COLUMN
00621 297* STEAM9= STRMM(1)*1.001 * 2000./HOUR *.1
00622 298* STEAM= STFAM + STFAM9
00623 299* AA(67,17) = STEAM9 *.1
00624 300* CALL HEATEX
00624 301* C
00624 302* C DISTILLATION COLUMN - MATERIAL BALANCE

```

Table I.--Continued.

```

00624 303* C
00625 304* STOP(1) = STRM(5,1) * .99887
00626 305* STOP(2) = STOP(1) * .1445
00627 306* SBOT(1) = STRM(5,1) * .00113
00630 307* SBOT(2) = STRM(4,1) - STOP(2)
00631 308* SBOT(3) = STRM(1,1) + STRM(1,2) + STRM(1,3) + (.001*STRMM(1))
00632 309* SBOT = SBOT(1) + SBOT(2) + SBOT(3)
C
00632 311* C DISTILLATION COLUMN
00632 312* C REBOILER
C
00633 314* STEAMR=AA(90,16) * FACT10*10709./50.
00634 315* AA(67,17) = .1* STEAMR
00635 316* CALL HEATEX
00636 317* STEAME= STEAM + STEAMR
00637 318* TANKAE= FACT10* AA(90,16)* 100./50.
C TANK ASSOCIATED WITH DISTILLATION COLUMN
00640 320* IA(40,1) = 1
00641 321* AA(40,17) = TANKA
00642 322* CALL STORAG
00643 323* WIDTHE= 4.* SQRT(AA(90,16)*FACT10/75.)
00644 324* I= WIDTH/2
00645 325* WIDTHE= 2*I
00646 326* IF(WIDTH.LT.4.001) WIDTH = 4.
00650 328* AA(43,18) = 24.
C AA(43,18) = THE TRAY SPACING IN INCHES
00651 329* AA(43,20) = WIDTH
00652 330* AA(43,17) = 54.
C AA(43,17) = THE COLUMN HEIGHT IN FEET
00653 332* AA(43,1) = .4
00654 333* CALL COLUMN
00655 334* IA(42,4) = 2
00656 335* IA(42,2) = 1
00657 336* IA(42,3) = 1
00660 337* AA(42,18) = WIDTH
00661 338* AA(42,19) = 54.
00662 339* CALL VESSEL
00663 340* LOPPS = LOPPS+5
00664 341* WASTE = (.00113*STRM(5,1)) + (.0001*(PRDCTA+PRDCTB))
00665 342* AA(40,17) = WASTE* 2000./ 8.33 * DAYSR
00666 343* IA(40,1) = n
00667 344* CALL STORAG
00670 346* LOPPS = LOPPS + 1
C IPA STORAGE TANK(MAKEUP IPA)
00670 347* C CONDENSER FOR DISTILLATION COLUMN
00671 348* WATER = 669.* FACT10* AA(90,16)/ 50.
00672 349* AA(67,17) = WATER* 8.33 * 60. * .01
00673 350* CALL HEATEX
00674 351* AA(66,17) = 1n5. * (AA(90,16)*FACT10/75.) * 20.
00675 352* CALL PMPCNT
00676 353* HP= 2.* (AA(90,16)* FACT10/75.)
00677 354* SUMHP = HP + SUMHP
C CENTRIFUGE SECTION
00677 355* MATRL = SBOT + AA(90,1A)
00700 356* OIL = STRM(1,1) + (AA(90,18)*XOIL)
00701 357* AA(40,17) = MATRL* 2000. / (HOUR*8.33)
00702 358* IA(40,1) = 1
00703 359*

```

Table I.--Continued.

```

00704 360* CALL STORAG
00705 361* AA(66,17) = 30.* AA(40,17)
00706 362* IA(66,1) = 0
00707 363* CALL PMPCNT
00710 364* SUMHP = SUMHP + 0.0015*AA(66,17)
00710 365* C NUMBER OF CENTRIFUGES
00711 366* HP = MATRL*.01* 2000./(HOUR*.8,33)
00712 367* N3 = (HP/20.) + 1.
00713 368* HP = 20* N3
00714 369* SUMHP = SUMHP + HP
00715 370* DO 47 I=1,N3
00720 371* AA(54,17) = 20.
00721 372* CALL CNTFGE
00722 373* 47 CONTINUE
00724 374* LOOPS = LOOPS + N3
00725 375* SAB = OIL * 1.1
00726 376* SCB = MATRL - OIL
00726 377* C SECOND CENTRIFUGE
00727 378* HP = SAB *.025* 2000./(HOUR*.24.)
00730 379* N2 = (HP/20.) + 1.
00731 380* HP = N2* 20
00732 381* SUMHP = SUMHP + HP
00733 382* DO 46 I=1,N2
00736 383* AA(52,17) = 20.
00737 384* CALL SHARP
00740 385* 46 CONTINUE
00742 386* HOTH20 = 0.1 * OIL
00742 387* C OIL STORAGE
00743 388* DAZOIL = 15.
00744 389* AA(40,17) = DAZOIL*OIL*2000./8.33
00745 390* IA(40,1) = 0
00746 391* CALL STORAG
00747 392* AA(66,17) = AA(40,17)*30./(60.*HOUR*DAZOIL)
00750 393* IA(66,1) = 0.
00751 394* CALL PMPCNT
00752 395* CALL PMPCNT
00753 396* SUMHP = SUMHP + (2.*AA(66,17)*.001)
00753 397* C DISSOLVED SOLIDS STREAM
00753 398* C
00754 399* C
00754 400* SBOT = SCB
00755 401* SBQQT = (STRM(2,1)+(XLIQD*X50L)) * 2.
00756 402* HWAT = SBOT - SBQQT
00757 403* IF(HWAT.GE.0.) GO TO 51
00761 404* PRINT 3006
00763 405* 3006 FORMAT(/50H FISH SOLIDABLES ARE MORE THAN 50 PERCENT PROTEIN )
00764 406* AA(90,4) = SBOT
00765 407* GO TO 52
00766 408* 51 CONTINUE
00767 409* AA(90,4) = SBQQT
00770 410* TONA = SBQQT/HOUR*2000.
00771 411* AA(33,17) = TONA/ 20.
00772 412* CALL EVPHOR
00773 413* CALL EVPHOR
00774 414* CALL EVPHOR
00775 415* SAQT = STPM(2,1)/0.3
00776 416* IF(SAQT.GE.SBOT) SAQT = SBOT

```

Table I.--Continued.

```

01000 417* AA(33,17) = SAQT * 2000. / (HOUR * 25.)
01001 418* STEAM = STEAM + (HWAT * 2000. / HOUR)
01002 419* CALL EUPHOR
01003 420* IA(66,1)=0.
01004 421* AA(66,17)=30.*SRQOT *2000./(10.*60.*HOUR)
01005 422* CALL PMPCNT
01006 423* HP=.001*AA(66,17)
01007 424* SUMHP=SUMHP + HP
01007 425* C
01007 426* C ACID MIX TANK
01007 427* C
01010 428* AA(40,17)=SRQOT *2000./(10.*1.)*.01
01011 429* IA(40,1)=2
01012 430* CALL STORAG
01013 431* IA(40,1)=0
01013 432* C
01013 433* C STORAGE OF FISH SOLUBILIS(15 DAYS)
01013 434* C
01014 435* IA(66,1)=0
01015 436* AA(66,17)=30.*AA(40,17)/(60.*HOUR)
01016 437* CALL PMPCNT
01017 438* HP=.001*AA(66,17)
01020 439* SUMHP=SUMHP + HP
01021 440* IA(40,1)=2
01022 441* AA(40,17)=SRQOT *2000./10. *15.
01023 442* CALL STORAG
01024 443* IA(40,1)=0.
01025 444* 52 CONTINUE
01025 445* C
01025 446* C ACID TANK AND FISH SOLUBILIS STORAGE
01025 447* C
01025 448* C
01025 449* C DRYING AND CONDITIONING OPERATION(SOLIDS FROM EXTRACTION VESSELS)
01025 450* C
01026 451* TASA= STMM(NOREAC+1)/2.
01027 452* NZ= NOREAC + 1
01030 453* TASB= STM(1,N7) + STM(2,N7) + STM(3,N7) + (0.05*STM(4,NZ))
01030 454* 1 + (STM(5,N7)*1.E-04 * 1.0 )
01031 455* TASC= STM(4,NZ) * .95
01032 456* TASD= STM(5,NZ) * .9999
01033 457* STEAM6 = (TASC + 1.0 * TASD) * 2000. / HOUR
01034 458* STEAM= STEAM + STEAM6
01034 459* C DRYER - CONDITIONFR
01035 460* AA(21,17) = 3.8* 16.* TASA/ 24.
01036 461* IA(21,5) = 6.
01037 462* BB(2) = 0.9
01040 463* CALL DRYERR
01041 464* BR(2) = 1.0
01042 465* IA(21,5) = 7
01043 466* CALL DRYERR
01044 467* BR(2) = 1.0
01045 468* IA(21,5) = 7
01046 469* CALL DRYERR
01047 470* IA(21,5) = 8
01050 471* BB(2) = 1.0
01051 472* CALL DRYERR
01052 473* LOOPS = LOOPS + 4

```

Table I.-- Continued.

```

01053 474* AA(17,18) = 6.
01054 475* AA(17,17) = 20.
01055 476* IA(17,5) = 1
01056 477* CALL SCREWDR
01057 478* C CONVEYER FOR MIL
01058 479* IF(IPTION(2),F0.3) GO TO 44
01059 480* AA(18,17) = (TASB/8.)
01060 481* CALL HAMMER
01061 482* HP = TASB * 2000. * 75. / (HOUR * 700.)
01062 483* SUMHP = SUMHP + HP
01063 484* PRDCTA = STM(2,NOREAC+1) + STM(3,NORFAC+1)
01064 485* PRDCTA = PRDCTA / 0.95
01065 486* PRDCTB = 0.
01066 487* AA(75,17) = PRDCTA * 2000. / (25. * HOUR * 60.)
01067 488* CALL BAGGMA
01068 489* CALL SCALE
01069 490* AA(75,17) = AA(75,17) * HOUR * 60.
01070 491* GO TO 49
01071 492* 44 CONTINUE
01072 493* C
01073 494* C AT THE TIME THIS CODE WAS COMPILED THERE IS NO SATISFACTORY METHOD
01074 495* C OF SEPARATING ASH AND DRY PROTEIN-- SPACE IS PROVIDED WHEN THIS
01075 496* C TECHNOLOGY BECOMES AVAILABLE
01076 497* C
01077 498* C 49 CONTINUE
01078 499* C BOILER
01079 500* AA(27,18) = 150.
01080 501* AA(27,17) = STFAM
01081 502* CALL BOILER
01082 503* IA(49,1) = 2
01083 504* AA(49,17) = STEAM * 1000. * HOUR / (8.33 * 140000.) * 15.
01084 505* CALL STORAC
01085 506* IA(66,1) = 0
01086 507* AA(66,17) = 30. * AA(40,17) / (60. * 15. * HOUR)
01087 508* CALL PMPCNT
01088 509* HP = .01 * AA(66,17)
01089 510* SUMHP = SUMHP
01090 511* C CONTROL LOOPS
01091 512* XLOOPS = L00PS
01092 513* COST(1) = XLOOPS * AA(100,1)
01093 514* COST(5) = COST(5)
01094 515* COSTA(1) = COSTA(1) + COST(1)
01095 516* COSTA(5) = COSTA(5) + COST(5)
01096 517* PRINT 1021, COST(1), COST(5)
01097 518* C FORK LIFT
01098 519* 1021 FORMAT(/25H CONTROL INSTRUMENTATION , 35X, F10.3, 30X, F10.3)
01099 520* COST(1) = AA(100,20)
01100 521* COST(5) = COST(1)
01101 522* COSTA(1) = COSTA(1) + COST(1)
01102 523* COSTA(5) = COSTA(5) + COST(5)
01103 524* PRINT 1022, COST(1), COST(5)
01104 525* AA(8,17) = T0MS
01105 526* CALL CONDEN
01106 527* 1022 FORMAT(/ 25H PAYLOADER , 10X, 25X, F10.3, 30X, F10.3)
01107 528* C
01108 529* C BOILER WATER TREATMENT
01109 530* C

```

Table I.--Continued.

01137	531*	COST(5)=1.	
01140	532*	COST(1)=COST(5)	
01141	533*	PRINT 4242, COST(1), COST(5)	
01145	534*	FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H	,10H
01145	535*	1 F10.3,F10.3)	
01146	536*	COSTA(1)=COSTA(1) + COST(1)	
01147	537*	COSTA(5)=COSTA(5) + COST(5)	
01147	538*	C SEA WATER PUMPS	
01147	539*	C	
01147	540*	C	
01150	541*	AA(90,10)=WATER*60. + 4.*STEAM	
01151	542*	AA(66,17) = AA(00,10)*1.2/60.	
01152	543*	IA(66,1)=1.	
01153	544*	IA(66,4)=2.	
01154	545*	CALL PMPCNT	
01155	546*	IA(66,1)=0	
01156	547*	IA(66,4)=0	
01157	548*	HP= .001*AA(66,17)	
01160	549*	SUMHP=SUM(HP + HP	
01160	550*	C CARBON ADSORBER	
01160	551*	C	
01160	552*	C	
01161	553*	COST(1)=2.	
01162	554*	COST(5)=COST(1)	
01163	555*	PRINT 4243, COST(1), COST(5)	
01167	556*	COSTA(1)=COSTA(1) + COST(1)	
01170	557*	COSTA(5)=COSTA(5) + COST(5)	
01171	558*	4243 FORMAT(/25H CARBON ADSORBER	, 10X ,15H
01171	559*	1 F10.3,30X,F10.3)	
01171	560*	C VENT CONDENSER	
01171	561*	C	
01171	562*	C	
01172	563*	AA(66,17)=20.	
01173	564*	IA(67,1)=1	
01174	565*	IA(67,4)= 4	
01175	566*	CALL HEATEX	
01176	567*	IA(67,1)=0	
01177	568*	IA(67,4)=0	
01200	569*	CALL SCALE	
01201	570*	CALL SCALE	
01202	571*	PRINT 1041,(COSTA(J),J=1,6)	
01210	572*	1041 FORMAT(/25H TOTAL COSTS	, 35X,6F10.3)
01211	573*	AA(100,2) = SUMHP*.7457 * 24.	
01212	574*	AA(100,10)= COSTA(5)	
01213	575*	AA(90,1) = STEAM*1000.*24./140000.	
01213	576*	C MATERIAL BALANCE	
01214	577*	AA(90,3) = PRDCTB	
01214	578*	AA(90,7) = PRDCTA	
01215	579*	AA(90,5)=011	
01216	580*	AA(90,18)=WASTE	
01217	581*	AA(90,19)=ACID	
01220	582*	CALL WATER(TONS)	
01221	583*	FISH = TONS*2000./24.	
01222	584*	PRINT 1003 , FISH	
01226	585*	FORMAT(/7X27H FISH TO EXTRACTION VESSELS,F8.0,7H LB/HR)	
01227	586*	YYA=STEAM1	
01230	587*	PRINT 1201,YYA	

Table I.-Continued.

01233	588*	1201	FORMAT(/8X,15H STEAM(STIRRED VESSEL 1)	,F8.0,7H LR/HR)
01234	589*		YYE=STEAM2	
01235	590*		PRINT 1202,YYR	
01240	591*	1202	FORMAT(/8X,15H STEAM(STIRRED VESSEL 2)	,F8.0,7H LR/HR)
01241	592*		YYE= STEAM3	
01242	593*	1203	FORMAT(/8X,15H STEAM(STIRRED VESSEL 3)	,F8.0,7H LR/HR)
01243	594*		YYD= STEAM4	
01244	595*		PRINT 1204,YYD	
01247	596*	1204	FORMAT(/8X,15H STEAM(STIRRED VESSEL 4)	,F8.0,7H LR/HR)
01252	597*		YYE = STEAM5	
01253	598*		PRINT 1205,YYF	
01254	599*	1205	FORMAT(/8X,15H STEAM(PREHEATER-DISTILLATION)	,F8.0,7H LR/HR)
01257	600*		YYG= STEAMR	
01260	601*		PRINT 1206,YYG	
01261	602*	1206	FORMAT(/8X,15H STEAM(REBOTLER)	,F8.0,7H LR/HR)
01264	603*		YYH = STEAM6	
01265	604*		PRINT 1207,YYH	
01266	605*	1207	FORMAT(/8X,15H STEAM(ROTARY DRYER FPC)	,F8.0,7H LR/HR)
01271	606*		YYI= STEAMW	
01272	607*		PRINT 1208,YYI	
01273	608*	1208	FORMAT(/8X,15H STEAM(ROTARY DRYER BONE MEAL	,F8.0,7H LR/HR)
01276	609*		YYJ=(STEAM*4.)	
01277	610*		PRINT 1209,YYJ	
01300	611*		YYK= WATER	
01303	612*		PRINT 1210,YYK	
01304	613*	1210	FORMAT(/8X,15H COOLING WATER DISTILLATION COND.	,F8.0,9H GAL/MIN)
01307	614*		YYL= STEAM	
01307	615*	1209	FORMAT(/8X,15H COOLING WATER CONDENSER	,F8.0,9H GAL/MIN
01310	616*		YYL= STEAM	
01310	617*		PRINT 1211,YYL	
01311	618*		FORMAT(/8X,15H TOTAL STEAM	,F8.0,7H LR/HR)
01312	619*		YYM = (STEAM*4.) + WATER	
01315	620*	1211	FORMAT(/8X,15H TOTAL WATER	,F8.0,7H LR/HR)
01316	621*		PRINT 1212,YYM	
01317	622*	1212	FORMAT(/8X,15H TOTAL WATER	,F8.0,7H LR/HR)
01322	623*		PRINT 1213	
01323	624*	1213	FORMAT(/40X, 9H STRAM 1,7X,9H STREAM 2,7X,9H STREAM 3,7X,9H STR	
01325	625*		CEAM 4,7X,9H STREAM 5,7)	
01325	626*		PRINT 1214,(STRM(1,K)*K=1,5)	
01326	627*		PRINT 1215,(STRM(3,K)*K=1,5)	
01334	628*		PRINT 1216,(STRM(2,K)*K=1,5)	
01342	629*		PRINT 1217,(STRM(4,K)*K=1,5)	
01350	630*		PRINT 1218,(STRM(5,K)*K=1,5)	
01356	631*		PRINT 1219,(STM (1,K)*K=1,5)	
01364	632*		PRINT 1220,(STM (3,K)*K=1,5)	
01372	633*		PRINT 1221,(STM (2,K)*K=1,5)	
01400	634*		PRINT 1222,(STM (4,K)*K=1,5)	
01406	635*		PRINT 1223,(STM (5,K)*K=1,5)	
01414	636*	1214	FORMAT(/10X20H RAFFINATE OIL	,10X,4(F10.3, AX),F10.3)
01422	637*	1215	FORMAT(/10X20H RAFFINATE ASH	,10X,4(F10.3, AX),F10.3)
01423	638*	1216	FORMAT(/10X20H RAFFINATE	,10X,4(F10.3, AX),F10.3)
01424	639*	1217	FORMAT(/10X20H RAFFINATE	,10X,4(F10.3, AX),F10.3)
01425	640*	1218	FORMAT(/10X20H RAFFINATE	,10X,4(F10.3, AX),F10.3)
01426	641*	1219	FORMAT(/10X20H RAFFINATE	,10X,4(F10.3, AX),F10.3)
01427	642*	1220	FORMAT(/10X20H EXTRACT	,10X,4(F10.3, AX),F10.3)
01430	643*	1221	FORMAT(/10X20H EXTRACT	,10X,4(F10.3, AX),F10.3)
01431	644*		FORMAT(/10X20H EXTRACT	,10X,4(F10.3, AX),F10.3)

Table I.-- Continued.

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01432 645* 1222 FORMAT(/10X,20H EXTRACT WATER ,F10X,4(F10.3, AX),F10.3)
01433 646* 1223 FORMAT(/10X,20H EXTRACT ALCOHOL ,F10X,4(F10.3, AX),F10.3)
01434 647* XXA= STMM(5)* 2000./24.
01435 648* PRINT 1224, XXA
01440 649* 1224 FORMAT(/8X,15H FLOW FROM EXTRACTION VESSEL 4 ,F8.0,7H LB/HR )
01441 650* XXB= STRMM(1)* 2000./24.
01442 651* 1225 FORMAT(/8X,15H FLOW FROM EXTRACTION VESSEL 1 ,F8.0,7H LB/HR )
01443 652* PRINT 1225, XXB
01446 653* XXC=MATRL*2000./HOUR
01447 654* PRINT 1226,XXC
01452 655* 1226 FORMAT(/8X,15H AQUEOUS STREAM(CENTRIFUGE) ,F8.0,7H LB/HR )
01453 656* XXD=(STOP(1)+STOP(2))*2000./24.
01454 657* PRINT 1227,XXD
01457 658* 1227 FORMAT(/8X,15H TOPS FROM DISTILLATION COLUMN ,F8.0,7H LB/HR )
01460 659* XXE= SPOTT*2000./24.
01461 660* PRINT 1228,XXE
01464 661* 1228 FORMAT(/8X,15H BOTTOMS FROM DISTILLATION COLUMN ,F8.0,7H LB/HR )
01465 662* XXG= AA(90,5)*2000./24.
01466 663* PRINT 1230,XXG
01471 664* 1230 FORMAT(/8X,15H FISH OIL PRODUCT ,F8.0,7H LB/HR )
01472 665* XXH=AA(90,3)*2000./24.
01473 666* 1231 FORMAT(/8X,15H FISH PROTEIN CONCENTRATE ,F8.0,7H LB/HR )
01474 667* XXI=AA(90,7)*2000./24.
01475 668* PRINT 1232, XXH
01500 669* PRINT 1231, XXI
01503 670* 1232 FORMAT(/8X,15H BONE MEAL CONCENTRATE ,F8.0,7H LB/HR )
01504 671* AA(95,1)=SB00T
01505 672* XXJ = AA(95,1)* 2000./24.
01506 673* PRINT 1233, XXJ
01511 674* 1233 FORMAT(/8X,15H FISH SOLUBLES ,F8.0,7H LB/HR )
01512 675* IXX=(14.0*(TONS/50.))*31 + 0.5
01513 676* AA(90,8)=IXX*8
01514 677* AA(90,9)=(YYJ+YYK)*24.
01515 678* AA(90,13) = AA(90,13) + (AA(90,3)+AA(90,7)+AA(90,20)+AA(90,4))
01516 679* RETURN
01517 680* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S BIOLOG*BIOLOG
FOR S9A-07/12-11:34 (0,)

SUBROUTINE BIOLOG ENTRY POINT 002304

STORAGE USED: CODE(1) 002350; DATA(0) 000733; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 PMPREC
0006 RELT
0007 STORAG
0010 REFRIG
0011 PMPCNT
0012 SILO
0013 BUCKET
0014 GRINDR
0015 REACTR
0016 AGITOR
0017 SCREWR
0020 SCREWR
0021 DRYERR
0022 HAMMER
0023 RAGGMA
0024 SCALE
0025 SHARP
0026 FVPFLM
0027 EVPSPR
0030 BOILER
0031 CONDEN
0032 WATER
0033 NRDC\$
0034 NI02\$
0035 NPRT\$
0036 NI01\$
0037 NEXP6\$
0040 FERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000367	160L	0000	000041	1000F	0000	000050	1001F	0000	000065	1002F	0000	000252	1003F
0000	000263	1604F	0000	000274	1005F	0000	000342	1006F	0000	000353	1007F	0000	000364	1008F
0000	000375	1609F	0001	000544	101L	0000	000406	1010F	0000	000417	1011F	0000	000430	1012F
0000	000441	1613F	0000	000442	1014F	0000	000305	1015F	0000	000463	1016F	0000	000474	1017F
0000	000505	1618F	0000	000516	1019F	0001	000627	1021F	0000	000527	1020F	0000	000207	1021F
0000	000225	1622F	0000	000546	1023F	0000	000551	1024F	0001	000712	103L	0000	000316	1033F
0000	000243	1641F	0001	000006	1066F	0000	000027	111F	0000	000327	111F	0001	000013	1146
0001	000020	1226	0000	000100	2000F	0001	000134	2016	0000	000113	3000F	0000	000171	4242F

Table I.-- Continued.

0000	000153	4249F	0001	001160	4706	0000	000031	5000F	0001	001234	5106	0001	001730	7076		
0001	001757	7226	0003	000000	AA	0000	R	000012	0003	R	004704	BB	0000	R	000024	COOL
0004	R	000000	COST	0004	R	000007	COSTA	0000	R	000023	FISH	0000	R	000002	GALLON	
0000	R	000003	GALS	0000	R	000007	HP	0000	I	000000	I	0000	I	000720	INJPS	
0000	I	000014	INST	0000	I	000025	IXX	0000	I	000022	J	0000	I	000005	NUM	
0000	R	000026	PXX	0000	R	000016	SLDS	0000	R	000004	SUMHP	0000	R	000011	TONSA	
0000	R	000015	VOLD	0000	R	000013	VOLT	0000	R	000017	WATER	0000	R	000021	XLOOPS	
0001	001757	7226	0003	000000	AA	0000	R	000012	0003	R	004704	BB	0000	R	000024	COOL
0004	R	000000	COST	0004	R	000007	COSTA	0000	R	000023	FISH	0000	R	000002	GALLON	
0000	R	000003	GALS	0000	R	000007	HP	0000	I	000000	I	0000	I	000720	INJPS	
0000	I	000014	INST	0000	I	000025	IXX	0000	I	000022	J	0000	I	000005	NUM	
0000	R	000026	PXX	0000	R	000016	SLDS	0000	R	000004	SUMHP	0000	R	000011	TONSA	
0000	R	000015	VOLD	0000	R	000013	VOLT	0000	R	000017	WATER	0000	R	000021	XLOOPS	
1*	00101															
2*	00103															
3*	00104															
4*	00105															
5*	00110															
6*	00111															
7*	00113															
8*	00116															
9*	00117															
10*	00121															
11*	00124															
12*	00126															
13*	00135															
14*	00136															
15*	00140															
16*	00141															
17*	00145															
18*	00147															
19*	00150															
20*	00154															
21*	00154															
22*	00155															
23*	00161															
24*	00161															
25*	00162															
26*	00164															
27*	00164															
28*	00165															
29*	00167															
30*	00167															
31*	00167															
32*	00167															
33*	00167															
34*	00167															
35*	00170															
36*	00171															
37*	00172															
38*	00173															
39*	00174															
40*	00175															
41*	00176															
42*	00177															
43*	00200															
44*	00203															
45*	00205															
46*	00206															

```

SUBROUTINE TIOLOG(TONS)
COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
COMMON /BLOCK2/ COST(7),COSTA(7)
DO 1 I=1,7
COST(I)=0.0
COSTA(I)=0.0
DO 2 I=1,20
AA(90,I)=0.0
AA(91,I)=0.0
DO 10 I=30,73
BB(I)=BB(I)*0.01
READ 111, BB(40),BR(41),BR(42),BR(43),BR(44)
FORMAT(5F12.5)
PRINT 5000
5000 FORMAT(7BX36H ANTIOXIDANT PRICE AND EFFECTIVENESS )
PRINT 1001, BR(44), BR(43)
PRINT 1000
1000 FORMAT(7BX31H ENZYME PRICE AND EFFECTIVENESS )
PRINT 1001, BR(41), BR(40)
1001 FORMAT(7BX8H PRIC =,F5.2,12H DOLLARS/LR,7F8.3,32H LA REQUIRED PF
CR 100 LR OF FISH )
IF (BR(42) .GT. 0.7) PRINT 1002, BR(42)
1002 FORMAT(7XF8.2,51H PERCENT OF DISSOLVED PROTEIN PACKAGED AS RCF PA
CSTE )
PRINT 2000
2000 FORMAT(1H1/55H DETAILED EQUIPMENT COSTS (A L COSTS IN 1000.0 DOL
CLARS) )
PRINT 3000
3000 FORMAT (/19H EQUIPMENT TYPE,10X10H CAPACITY,12X9H MATERIAL,
C60H RASE MATERIALS LABOR INDIRECT MODULE
C0X60H COST COSTS COSTS COSTS COSTS
C UNLOADING AND STORAGE OF FISH
C
TONSA=TONS*2000./A.33
GALLONE=TONSA/(24.*60.)
GALS=GALLON*1.3
SUMHP=0.
IA(65,1)=0
IA(65,2)=1.0
AA(65,17)=GAL S*30.
NUM=TONS/500 + 1
DO 143 I=1,NUM
CALL PHMPREC
IA(65,2)=0.0
SUMHP=SUMHP+(AA(65,17)*.001*1.5)

```

Table I.-- Continued.

```

00207 47* SUMHP= SUMHP +(AA(65,17)*.001*1.5)
00210 48* IF(TONSA.LT.30000.) G=(30000./24.*60.)*15.
00212 49* IF(TONSA.GE.30000.) G=(450000./24.*60.)*15.
00214 50* IF(TONS.LE.150.) AA(70,1A)= 36.
00216 51* IF(TONS.GT.150.) AA(70,1A)= 48.
00220 52* AA(70,17)=100.
00221 53* CALL BELT
00222 54* HP = TONS*0.00124 +13.6
00223 55* SUMHP = HP + SUMHP
00224 56* AA(40,17)=30.0*TONS
00225 57* IA(40,1)=0.0
00226 58* IA(40,2)=2
00227 59* CALL STORAG
00230 60* IA(40,2)=0
00231 61* AA(85,17)=0.5*TONS**1.0
00232 62* IA(85,1) =30
00233 63* CALL REFRIG
00234 64* SUMHP = SUMHP + 4.7*AA(85,17)
00235 65* COST(1)=1.19
00236 66* IF(TONS.GE.300) COST(1)=1.88
00240 67* COST(5)=COST(1)
00241 68* PRINT 4249, COST(1), COST(5)
00245 69* COSTA(1)=COSTA(1)+COST(1)
00246 70* COSTA(5)=COSTA(5)+COST(5)
00247 71* FORMAT(25H BRINE MAKE-UP+SALT STOR., 10X ,15H
00247 72* ,F10.3,30X,F10.3)
00247 73* C PUMP FOR BRINE MAKE-UP (RRONZF)
00250 74* IA(66,1)=1
00251 75* AA(66,17)=TONS*3.*2000./24.*60.*62.4)*.69*7.75
00252 76* CALL PMPCNT
00253 77* IA(66,1)=0
00254 78* HP=.001*AA(66,17)
00255 79* SUMHP=SUMHP+HP
00256 80* C PUMP FOR WATER INTO BRINE MAKE-UP
00257 81* AA(66,17)=AA(66,17)*.917
00260 82* IA(66,1)=0
00261 83* CALL PMPCNT
00262 84* HP=.001*AA(66,17)
00262 85* SUMHP=SUMHP+HP
00262 86* C FISH STORAGE FOR 3 DAYS
00262 87* C
00263 88* IA(7,1)=1
00264 89* AA(7,17)=3.*TONS*2000.*1.69/62.4
00265 90* CALL SILO
00266 91* LOOPS=0.0
00267 92* LOOPS=LOOPS+1.
00270 93* CALL SILO
00271 94* TONG=TONS/24.
00272 95* AA(71,18)= TONG
00273 96* AA(71,17)= 20.
00274 97* CALL BUCKET
00275 98* HP = TONS*0.00106
00276 99* SUMHP = HP + SUMHP
00276 100* C FISH GRINDING AND DIGESTION
00276 101* C
00276 102* C
00276 103* C

```

Table I.--Continued.

```

00277 104* IF(TONSG.LT. 3) AA(50,17)=3
00301 105* IF(TONSG.GT. 6) AA(50,17)=6
00303 106* IF(AA(50,17).GT. 0.0) CALL GRINDR
00305 107* TONSG = TONSG-AA(50,17)
00306 108* IF(TONSG.GT. 0.2) GO TO 100
00310 109* HP = 40*TONSG/3
00311 110* SUMHP=HP+SUMHP
00311 111* C PUMP AFTER GRINDER
00312 112* AA(66,17)=30.*TONS*2000./(24.*60.*8.33)
00313 113* IA(66,1)=0
00314 114* CALL PMPCNT
00315 115* SUMHP=SUMHP+.001*AA(66,17)
00316 117* CALL PMPCNT
00317 118* SUMHP=.001*AA(66,17)+SUMHP
00320 119* AA(40,17) = 2*TONS*2000./(8.33*24)
00321 120* IA(40,1) = 1
00322 121* CALL STORAG
00323 122* IA(40,1) = 0
00324 123* AA(90,15)=TONS*.0004
00325 124* AA(90,13)=(BR(30)+BR(31)+BR(32))*TONS*.0001
00326 125* AA(90,17)=TONS*.0432
00327 126* AA(90,14)=TONS*.0192
00330 127* AA(90,12)=TONS*(BR(40)/100.0)
00331 128* ADOT=0.0
00332 129* ADDT=AA(90,12)+AA(90,13)+AA(90,15)+AA(90,17)+AA(90,14)
00333 130* AA(91,1)=ADOT+.2*TONS
00334 131* VOLT=AA(91,1)*2000./(8.33*4.8)
00335 132* AA(51,2) = 2.0
00336 133* AA(51,17) = 2.0
00337 134* AA(49,17)=VOLT/3
00340 135* IF(AA(49,17).LT. 10000) AA(73,17) = AA(49,17)*0.005
00342 136* IF(AA(49,17).LT. 10000) GO TO 101
00344 137* IF(AA(49,17).GT. 10000) AA(73,17) = 50.
00346 138* IF(AA(49,17).GT. 10000) AA(49,17)=10000
00350 139* AA(66,17)=30.*AA(49,17)*4.8/(60.*24.)
00351 140* IA(66,1)=0
00352 141* CALL REACTR
00353 142* CALL AGITOR
00354 143* CALL SCREEN
00355 144* CALL REACTR
00356 145* CALL AGITOR
00357 146* CALL SCREEN
00360 147* CALL REACTR
00361 148* CALL AGITOR
00362 149* CALL SCREEN
00363 150* INST = 3
00364 151* HP = 3*AA(73,17)
00365 152* SUMHP = HP + SUMHP
00366 153* VOLT =VOLT -AA(49,17)*3
00367 154* IF(VOLT.LT. 500) GO TO 103
00371 155* IF(VOLD.LI. 10000) AA(49,17)=VOLD
00373 156* IF(AA(49,17).LT. 10000) AA(73,17) = AA(49,17)*0.005
00375 157* IF(VOLD.GT. 10000) AA(49,17)=10000
00377 158* IF(AA(49,17).GT. 10000) AA(73,17) = 50.
00401 159* CALL REACTR
00402 160* CALL AGITOR

```

Table I.--Continued.

00403	161*	CALL SCREEN
00404	162*	INST = INST + 1
00405	163*	VOLD = VOLD -AA(40,17)
00406	164*	HP = AA(73,17)
00407	165*	SUMHP = HP + SUMHP
00410	166*	GO TO 102
00411	167*	CONTINUE
00411	168*	103
00411	169*	C BONE FEED STREAM
00411	170*	C
00412	171*	BB(2)=1.
00413	172*	SLDS=((40./667.)*PB(31))+((110./250.)*BR(32))+((10./500.)*BR(30))
00413	173*	C)*TONS+((125./299.)*ADDI*(110./250.))
00414	174*	WATER=TONS*(1.+BR(31)+(174.3/299.3)*ADDI
00415	175*	AA(91,10)=((180./667.)*BR(31))+((112./500.)*BB(30))+((50./250.)*B
00415	176*	CB(32))*TONS+((125./299.3)*ADDI*(50./250.))+((1058./7216.5)*WATER)
00416	177*	AA(91,2)=(320./160.)*SLDS
00416	178*	C PUMP FOR SLUDGE FROM CFNTRIFUGE
00417	179*	IA(66,1)=0
00420	180*	AA(66,17)=AA(91,10)*30.*2000./124.*8.33*60.)
00421	181*	CALL PMPCNT
00422	182*	HP=.001*AA(66,17)
00423	183*	SUMHP=HP+SUMHP
00423	184*	C SCREW CONVEYOR
00423	185*	C
00424	187*	AA(17,18)=6
00424	188*	C FISH OIL STREAM
00424	189*	C
00425	190*	AA(91,3)=AA(91,1)-AA(91,2)
00425	191*	C PUMPS BEFORE AND AFTER HOLD TANK OF FIRST CENTRIFUGE
00426	192*	IA(66,1)=0
00427	193*	AA(17,17)=20
00430	194*	IA(17,5)=1
00431	195*	CALL SCREW
00432	196*	IA(21,5)=3
00433	197*	AA(21,17)=AA(91,2)*2.5
00434	198*	CALL DRYERR
00435	199*	AA(90,3)=(SLDS+AA(91,10)-((1058./7216.5)*WATER))/9
00436	200*	AA(91,12)=AA(91,2)+AA(91,10)-AA(90,3)
00436	201*	C
00436	202*	C BAGGING MACHINE FOR BONE MEAL
00436	203*	C
00437	204*	AA(75,17)=AA(90,3)*2000./124.*60.*25.)
00440	205*	IA(75,2)=0
00441	206*	IA(75,1)=0
00442	207*	AA(18,17)=AA(90,3)/24.
00443	208*	CALL HAMMER
00444	209*	CALL BAGGMA
00445	210*	AA(75,5)=AA(75,17)
00446	211*	AA(72,17) = 18.
00447	212*	CALL SCALE
00447	213*	C
00450	214*	AA(66,17)=AA(91,3)*30.*2000./124.*8.33*24.*60.)
00451	215*	CALL PMPCNT
00452	216*	CALL PMPCNT
00453	217*	SUMHP=2.*.001*AA(66,17)+SUMHP

Table I.--Continued.

```

00454 218* AA(72,17)=18.
00455 219* CALL SCALE
00456 220* AA(40,17) = AA(91,3)*2000./ (8.33*24.)
00457 221* IA(40,1) = 1
00460 222* CALL STORAG
00461 223* IA(40,1) = 0
00462 224* AA(91,6) = ((447./667.) * BB(31)) + ((3./500.) * BB(30)) + ((90./250.) * BB(3
00463 225* C21)) * TONS + ((125./209.3) * ANNT * (90./250.)) + ((15098./7216.5) * WATER)
00464 226* AA(91,4) = AA(01,3) - AA(91,6) - AA(91,10)
00465 227* HP = 0.01 * AA(91,3) * 2000.0 / (8.33 * 24.0)
00466 228* SUMHP = HP + SUMHP
00467 229* NUM = HP / 20. + 1
00472 230* DO 20 I=1,NUM
00473 231* AA(52,17) = 20.
00475 232* CALL SHARP
00476 233* HP = 0.025 * AA(91,4) * 2000.0 / (8.33 * 24.0)
00477 234* SUMHP = SUMHP + HP
00478 235* IA(66,1) = 0
00500 236* AA(66,17) = AA(91,4) * 2000. * 30. / (8.33 * 24. * 60.)
00501 237* CALL PMPCNT
00502 238* CALL PMPCNT
00503 239* SUMHP = 2. * * .001 * AA(66,17) + SUMHP
00504 240* AA(40,17) = AA(91,4) * 2000. / (8.33 * 24.)
00505 241* CALL STORAG
00506 242* NUM = HP / 20. + 1
00507 243* DO 30 I=1,NUM
00512 244* AA(52,17) = 20.0
00513 245* CALL SHARP
00513 246*
00513 247*
00513 248* C HOLD TANK FOR FISH OIL
00513 249* C
00515 250* AA(90,5) = TONS * BB(30) * .75
00516 251* AA(40,17) = AA(90,5) * 2000. / (8.33 * 24.)
00517 252* CALL STORAG
00517 253* C
00517 254* C FISH OIL STORAGE (15 DAYS)
00517 255* C
00520 256* AA(40,17) = 15. * AA(90,5) * 2000. / 8.33
00521 257* IA(40,1) = 0.0
00522 258* CALL STORAG
00523 259* AA(66,17) = AA(90,5) * 30. * 0.0 * 2000.0 / (8.33 * 24 * 60)
00524 260* SUMHP = SUMHP + (AA(66,17) * 0.001)
00525 261* SUMHP = SUMHP + (AA(66,17) * 0.001)
00526 262* IA(66,1) = 0
00527 263* CALL PMPCNT
00530 264* CALL PMPCNT
00530 265* C DISSOLVED SOLIDS STREAM
00530 266* C
00530 267* C PUMPS BEFORE AND AFTER HOLD TANK
00530 268* IA(66,1) = 0
00532 269* AA(66,17) = AA(91,6) * 2000. / (8.33 * 24. * 60. * 30.
00533 270* CALL PMPCNT
00533 271* CALL PMPCNT
00534 272* SUMHP = SUMHP + 2. * * .001 * AA(66,17)
00535 273* CALL PMPCNT
00536 274* AA(40,17) = AA(91,6) * 2000. / (8.33 * 24.)

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Table I.--Continued.

```

00537 275* IA(40,1) = 1
00540 276* CALL STORAG
00541 277* IA(40,1) = 0
00542 278* WATEVP=(5998./7216.5)*WATER-(AA(91,6)-(5998./7216.5)*WATER)
00543 279* AA(91,13)=WATEVP
00544 280* AA(31,17)=AA(91,17)*2000./ (24*25)
00545 281* CALL EVPFLM
00546 282* AA(91,7)=2.*(AA(91,6)-(5998./7216.5)*WATER)
00547 283* AA(90,6)=AA(91,7)*BR(42)*0.01
00550 284* AA(72,17) = 18.
00551 286* CALL SCALE
C
00551 287* C HOLD TANK
C
00551 288*
00552 289* AA(40,17)=AA(91,7)*2000./ (8.33*24.)*1.
00553 290* IA(40,1)=1
00554 291* CALL STORAG
00555 292* IA(40,1)=0
00556 293* C PUMP AFTER WIPE FILM FVAPORATOR
00556 294* IA(66,1)=0
00557 295* AA(66,17)=AA(91,7)*2000.*30./ (8.33*24.*60.)
00560 296* CALL PMPCNT
00561 297* HP=.001*AA(66,17)
00562 298* SUMHP=HP+SUMHP
00563 299* C PUMP BEFORE CANNING MACHTNE
00563 300* AA(66,17)=AA(90,6)*2000.*30./ (8.33*24.*60.)
00564 301* IF (BB(42).GT.0.0) CALL PMPCNT
00566 302* HP=.001*AA(66,17)
00567 303* SUMHP=HP+SUMHP
00570 304* AA(75,17)=AA(90,6)*2000.*30./ (8.33*24.*60.*0*5.0)
00571 305* IA(75,1)=1.0
00572 306* IA(75,2)=2.0
00573 307* IF (BB(42) .GT. 0.0) CALL RAGGNA
00575 308* IA(75,1) = 0.0
00576 309* AA(75,4)=AA(75,17)
00577 310* AA(75,4)=AA(75,4)*60.*24.
00600 311* IA(75,2)=0.0
00601 312* AA(91,9)=AA(91,7)-AA(90,6)
00601 313* C PUMP BEFORE SPRAY DRYER
00602 314* AA(66,17)=AA(91,9)*2000.*30./ (8.33*60.*24.)
00603 315* CALL PMPCNT
00604 316* HP=.001*AA(66,17)
00605 317* SUMHP=HP+SUMHP
00606 318* AA(90,7)=AA(91,9)/(2.*.95)
00607 319* AA(91,14)=AA(91,9)-AA(90,7)
00610 320* AA(30,17)=AA(91,14)*2000./24.0
00611 321* CALL EVPSPR
00612 322* AA(72,17) = 18.
00613 323* CALL SCALE
00614 324* IA(75,1)=0.
00615 325* IA(75,2)=0.
00616 326* AA(75,17)=AA(90,7) *2000./ (24*60*25)
00617 327* IF (BB(42) .GT. 100) CALL RAGGNA
00621 328* AA(75,17)=AA(75,17)+AA(75,5)
00622 329* AA(75,17)=AA(75,17)*60.*24.
C
00622 330* C SUMMATION OF STEAM,WATER AND FLECTICITY
00622 331*

```

Table I.--Continued.

00622	332*	C			
00623	333*		AA(91,15)=(AA(91,11)+AA(91,12)+AA(91,13)+AA(91,14))*1.05		
00624	334*		AA(27,17)=AA(91,15)*2000.0/24		
00624	335*	C	C BOILER WATER TREATMENT		
00624	336*	C			
00624	337*		COST(5)=1.000		
00625	338*		COST(1)=COST(5)		
00626	339*		PRINT 4242,COST(1),COST(5)		
00627	340*		COSTA(1)=COSTA(1)+COST(1)		
00633	341*		COSTA(5)=COSTA(5)+COST(5)		
00634	342*		FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H		,10H
00635	343*	1	,F10.3,30X,F10.3)		
00635	344*	C	C SEA WATER PUMPS		
00635	345*				
00635	346*	C			
00635	347*		AA(90,10)=33.1*(AA(91,13)+AA(91,14))*1.2		
00636	348*		AA(66,17)=AA(90,10)*2000.0/(8.33*24*60*0.066)		
00637	349*		IA(66,11)=1		
00640	350*		IA(66,4)=2		
00641	351*		CALL PMPCNT		
00642	352*		IA(66,1)=0		
00643	353*		IA(66,4)=0		
00644	354*		CALL BOILER		
00645	355*	C	C FUEL OIL STORAGE (15 DAYS)		
00645	356*	C			
00645	357*		IA(40,1)=2		
00645	358*		AA(40,17)=AA(27,17)/8.33*24**0.112*15.		
00646	359*		CALL STORAG		
00650	361*		IA(66,1)=0		
00651	362*		AA(66,17)=30.*AA(40,17)/(15.*60.*24.)		
00652	363*		CALL PMPCNT		
00653	364*		HP=.001*AA(66,17)		
00654	365*		SUMHP=SUMHP+HP		
00655	366*		SUMHP = SUMHP+(AA(66,17)*.001*1.5)		
00656	367*		AA(90,9)=4.*TONS+(174.3/299.3)*ADD1+.1*AA(91,4)+.1*AA(91,15)		
00657	368*		XLOOPS=LOOPS+10.+3.*TNST		
00660	369*		COST(1)=XLOOPS.*AA(100,1)		
00661	370*		COST(5)=COST(1)		
00662	371*		COSTA(1) = COSTA(1) + COST(1)		
00663	372*		COSTA(5)=COSTA(5) + COST(5)		
00664	373*		PRINT 1021,COST(1),COST(5)		
00665	374*		FORMAT(/ 25H CONTROL INSTRUMENTATION , 10X ,15H		,10H
00671	375*	1	,F10.3,30X,F10.3)		
00671	376*		AA(8,17) = TONS		
00672	377*		CALL CONDEN		
00673	378*		COST(1)=AA(100,2)		
00674	379*		COST(5)=COST(1)		
00675	380*		COSTA(1)=COST(1) + COSTA(1)		
00676	381*		COSTA(5)=COSTA(5) + COST(5)		
00677	382*		PRINT 1022,COST(1),COST(5)		
00700	383*		FORMAT(/ 25H PAYLOADER AND FORK LIFT , 10X ,15H		,10H
00704	384*	1	,F10.3,30X,F10.3)		
00704	385*		PRINT 1041,(COSTA(J),J=1.6)		
00705	386*		FORMAT(/25H TOTAL COSTS		
00713	387*		COSTA(7)=0.02*COSTA(1)		,35X6F10.3)
00714	388*				

Table I.-- Continued.

00715	389*		AA(100,10)=COSTA(5)	
00715	390*	C		
00715	391*	C	MATERIAL BALANCE INFORMATION PRINTOUT. ALL STREAMS HERE CONVERTED TO	
00715	392*	C	LB/HR	
00716	393*		AA(90,2)=SIMHP*.7457*24.	
00717	394*		AA(90,10)=AA(90,10)/R.33*2000./24.	
00720	395*		CALL WATER(TONS)	
00721	396*		DO 40 I=1,20	
00724	397*		AA(90,I)=AA(90,I)*2000/24	
00725	398*		AA(91,I)=AA(91,I)*2000/24	
00727	399*		FISH=TONS*2000/24	
00730	400*		PRINT 1003,FISH	
00733	401*	1003	FORMAT(/8X26H FISH FEED TO GRINDERS	,F8.0,7H LB/HR)
00734	402*		PRINT 1004,AA(90,12)	
00737	403*	1004	FORMAT(/8X26H ENZYMF TO DIGESTERS	,F8.2,7H LB/HR)
00740	404*		PRINT 1005,AA(90,15)	
00743	405*	1005	FORMAT(/8X26H,CAOH TO DIGESTERS	,F8.0,7H LB/HR)
00744	406*		PRINT 1015,AA(90,13)	
00747	407*	1015	FORMAT(/8X26H ANTI-OXIDANT TO DIGESTERS	,F8.2,7H LB/HR)
00750	408*		PRINT 1033,AA(90,17)	
00753	409*	1033	FORMAT(/8X26H 5N NAOH TO DIGESTERS	,F8.2,7H LB/HR)
00754	410*		PRINT 1111,AA(90,14)	
00757	411*	1111	FORMAT(/8X41H CONCENTRATED SULFURIC ACID TO DIGESTERS	,F8.2,7H LB/
00757	412*		CHR)	
00760	413*		PRINT 1006,AA(91,2)	
00763	414*	1006	FORMAT(/8X26H FEED TO ROTARY DRYER	,F8.0,7H LB/HR)
00764	415*		PRINT 1007,AA(91,12)	
00767	416*	1007	FORMAT(/8X26H ROTARY DRYER STEAM	,F8.0,7H LB/HR)
00770	417*		PRINT 1008,AA(90,3)	
00773	418*	1008	FORMAT(/8X26H BONF FEED	,F8.0,7H LB/HR)
00774	419*		PRINT 1009,AA(91,3)	
00777	420*	1009	FORMAT(/8X26H DIGESTER LIQUOR	,F8.0,7H LB/HR)
01000	421*		PRINT 1010,AA(90,5)	
01003	422*	1010	FORMAT(/8X26H FISH OIL	,F8.0,7H LB/HR)
01004	423*		PRINT 1011,AA(91,6)	
01007	424*	1011	FORMAT(/8X26H FEED TO FILM EVAPORATOR	,F8.0,7H LB/HR)
01010	425*		PRINT 1012,AA(91,13)	
01013	426*	1012	FORMAT(/8X26H FILM EVAPORATOR STEAM	,F8.0,7H LB/HR)
01014	427*		COOL=AA(91,13)*4	
01015	428*		PRINT 1013,COOL	
01020	429*	1013	FORMAT(/8X26H FILM EVAPORATOR COOLING	,F8.0,7H GAL/HR)
01021	430*		PRINT 1014,AA(91,7)	
01025	432*	1014	FORMAT(/8X26H BFC PASTE	,F8.0,7H LB/HR)
01026	433*		AA(90,13) = 0.0005*(AA(91,7) +AA(90,3))	
01031	434*	1016	FORMAT(/8X26H PACAGFD AS BFC PASTE	,F8.0,7H LB/HR)
01032	435*		PRINT 1017,AA(91,9)	
01035	436*	1017	FORMAT(/8X26H FEED TO SPRAY EVAPORATOR	,F8.0,7H LB/HR)
01036	437*		PRINT 1018,AA(91,14)	
01041	438*	1018	FORMAT(/8X26H SPRAY EVAPORATOR STEAM	,F8.0,7H LB/HR)
01042	439*		COOL=4*AA(91,14)	
01043	440*		PRINT 1019,COOL	
01046	441*	1019	FORMAT(/8X26H SPRAY EVAP. COOLING	,F8.0,7H GAL/HR)
01047	442*		PRINT 1020,AA(90,7)	
01052	443*	1020	FORMAT(/8X26H BFC POWDER	,F8.0,7H LB/HR,)
01053	444*		AA(91,16)=AA(91,15)+AA(91,13)-AA(91,14)-AA(91,12)	
01054	445*		PRINT 1023,AA(91,16)	

Table I.--Continued.

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01057 446* 1023 FORMAT(/8X26H MISCELLANEOUS STEAM ,F8.0,7H LB/HR )
01060 447* AA(90,9)=AA(90,9)/8.33
01061 448* PRINT 1024 ,AA(90,9)
01064 449* FORMAT(/8X26H CITY WATER ,F8.0,7H GAL/HR )
01065 450* AA(90,1) = AA(27,1)*24*0.0112
01066 451* AA(90,2) = SIMHP* .7457 * 24.
01067 452* AA(90,3) = AA(90,3)*24/2000
01070 453* AA(90,5) = AA(90,5)*24/2000
01071 454* AA(90,6) = AA(90,6)*24/2000
01072 455* AA(90,7) = AA(90,7)*24/2000
01073 456* IXX =(14.0*(TONS/50.0)**.31) +0.5
01074 457* PXX =IXX
01075 458* AA(90,8) =IXX*8.0
01076 459* AA(90,9) =AA(90,9)*24
01077 460* AA(90,12)=AA(90,12)*24
01100 461* AA(90,13)=AA(90,13)*24
01101 462* AA(90,15)=AA(90,15)*24
01102 463* AA(90,14)=AA(90,14)*24
01103 464* AA(90,17)=AA(90,17)*24
01104 465* RETURN
01105 466* END

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END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S XXIPA,XXIPA
FOR S9A-07/12-11:94 (0,)

SUBROUTINE XXIPA ENTRY POINT 004256

STORAGE USED: CODE(1) 004346; DATA(0) 001463; BLANK COMMON(2) 000000

COMMON RLOCKS:

0003 RLOCK1 005050
0004 RLOCK2 000016
0005 RLOCK4 000012

EXTERNAL REFERENCES (BLOCK, NAME)

0006 PMPREC
0007 HELT
0010 STORAG
0011 REFRIG
0012 SILO
0013 PMPCNT
0014 BUCKET
0015 PULVER
0016 AGITOR
0017 REACTR
0020 SCREEN
0021 SCREWR
0022 HEATEX
0023 DRYERR
0024 HAMMER
0025 BAGGMA
0026 CNTFGE
0027 SHARP
0030 VESSEL
0031 COLUMN
0032 EVPHOR
0033 BOILER
0034 CONDEN
0035 SCALE
0036 MATER
0037 NPRT\$
0040 NI02\$
0041 NI01\$
0042 SGR1
0043 NEXP6\$
0044 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

Block	Type	Relative Location	Name
0001	0000	000477 1003F	0001
0000	0001	002322 1044G	0001
0000	0001	002566 1142G	0001
0000	0000	000546 1204F	0000
0001	0000	000527 101L	0000
0000	0000	002374 1063G	0000
0000	0000	000014 116G	0000
0000	0000	000560 1205F	0000
000421	1022F	000410 1021F	0000
000246	1113F	000365 1110F	0000
000522	1202F	000510 1201F	0000
000604	1207F	000572 1206F	0000

Table I.--Continued.

0000	000616	1208F	0000	000642	1209F	0000	000630	1210F	0000	000654	1211F	0000	000666	1212F
0000	000700	1213F	0000	000716	1214F	0000	000727	1215F	0000	000740	1216F	0000	000751	1217F
0000	000762	1218F	0000	000773	1219F	0000	001004	1220F	0000	001015	1221F	0000	001026	1222F
0000	001037	1223F	0000	001050	1224F	0000	001062	1225F	0000	001074	1226F	0000	001106	1227F
0000	001120	1228F	0000	001132	1229F	0000	001144	1230F	0000	001156	1231F	0000	001170	1232F
0000	001202	1233F	0001	000041	1236	0000	000046	140G	0001	003504	1442G	0001	003713	1566G
0001	003724	1574G	0001	003735	1602G	0001	003746	1610G	0001	003757	1616G	0001	003770	1624G
0001	000114	1636	0001	004001	1632G	0001	004012	1640G	0001	004023	1646G	0001	004034	1654G
0000	000263	2000F	0001	000406	300G	0001	002105	300L	0000	000276	3001F	0000	000376	3006F
0001	000475	320G	0001	000517	320G	0001	000652	402G	0001	000653	405G	0001	000670	413G
0001	000673	420G	0000	000433	4242F	0000	000451	4243F	0000	000336	4249F	0001	001241	44L
0001	001015	453G	0001	003264	48L	0001	002161	49L	0001	003016	51L	0001	001231	517G
0001	003164	52L	0001	001263	535G	0001	001366	573G	0001	001372	577G	0003	R	000000 AA
0000	R	000165	AABAG	0000	R	000143	ABC	0000	R	000167	ACID	0004	R	000000 COST
0004	R	000007	COSTA	0000	R	000144	DX	0000	R	000146	FF	0000	R	000177 FT
0000	R	000112	G	0000	R	000127	GAA	0000	R	000170	GAL	0000	R	000107 GALS
0000	R	000172	HOP	0000	R	000113	HP	0000	R	000211	HWAT	0000	I	0003720 TA
0000	R	000426	INJPS	0000	I	000130	IP	0005	I	000000	TPTION	0000	I	000134 TR
0000	I	000135	IPR	0000	T	000140	IU	0000	I	000245	IXX	0000	I	000122 K
0000	I	000103	LOOPS	0000	T	000120	NA	0000	I	000117	NB	0000	I	000174 N2
0000	I	000201	N3	0000	R	000143	PRDCTA	0000	R	000102	PRDCTB	0000	R	000171 SAA
0000	R	000173	SAB	0000	R	000117	SAG	0000	R	000213	SAQT	0000	R	000077 SBOT
0000	R	000200	SBOTT	0000	R	000216	SBQGT	0000	R	000207	SBQT	0000	R	000153 STEAM3
0000	R	000202	STEAMR	0000	R	000214	STEAMW	0000	R	000257	STEAM1	0000	R	000150 STEAM3
0000	R	000151	STEAM4	0000	R	000140	STEAM6	0000	R	000176	STEAM9	0000	R	000062 STMM
0000	R	000123	STON	0000	R	000074	STOP	0000	R	000031	STRM	0000	R	000110 SUMHP
0000	R	000136	TANK	0000	R	000203	TANKA	0000	R	000154	TASA	0000	R	000156 TASC
0000	R	000157	TASD	0000	R	000212	TONA	0000	R	000105	TONSA	0000	R	000114 TONSG
0000	R	000132	VES	0000	R	000133	VESS	0000	R	000205	WATER	0000	R	000204 WIDTH
0000	R	000164	XAA	0000	R	000141	XIP	0000	R	000142	XIR	0000	R	000215 XLOOPS
0000	R	000233	XXA	0000	R	000234	XXR	0000	R	000235	XXC	0000	R	000237 XXE
0000	R	000240	XXF	0000	R	000241	XXG	0000	R	000242	XXH	0000	R	000244 XXJ
0000	R	000217	YYA	0000	R	000220	YYB	0000	R	000221	YYC	0000	R	000223 YYE
0000	R	000224	YYG	0000	R	000225	YYH	0000	R	000226	YYI	0000	R	000230 YYK
0000	R	000231	YYL	0000	R	000232	YYM	0000	R	000115	7A1	0000	R	000116 7A3
0000	R	000161	ZAT	0000	R	000162	ZAR							

SUBROUTINE XXIPA(TONS)

1* C ISOPROPYL ALCOHOL EXTRACTION PROCFS5

2* C

3* C

4* C

5* C

6* C

7* C

8* C

9* C

10* C

11* C

12* C

13* C

14* C

15* C

16* C

17* C

COMMON/BLOCK1/ AA(100,20),IA(100,5),BR(100)
COMMON/BLOCK2/ COST(7),COSTA(7)
COMMON/BLOCK4/ IPTION(10)
DIMENSION STM(5,5),STRW(5,5) , STMM(5) , STRMM(5)
DIMENSION STOP(3),SBOT(3)
AA(72,17)=1R.
PRDCTB=0.

1113 FORMAT(/ 25H WET MONOMER
,6F10.3)
C
IPTION(2)=IPTION(1)
LOOPS=0
DO 1 I=1,7

,F10.3,25H TONS

SST

Table I.-- Continued.

```

00120 18* COST(I)=0.0
00121 19* COSTA(I)=0.0
00123 20* IF(IPTION(I),E0.2) PRINT I120
00126 21* IF(IPTION(I),E0.1) PRINT I110
00131 22* DO 2 I= 1,20
00134 23* AA (90,I)=0.0
00135 24* AA (91,I)=0.0
00137 25* DO 10 I =30,30
00142 26* BB(I)=BB(I)*.01
00144 27* PRINT 2000
00146 28* FORMAT(HI)/55H DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL
00147 29* CLARS )
00147 30* PRINT 3001
00151 31* FORMAT (/1RH EQUIPMENT TYPF,10X10H CAPACITY,12X0H MATERIAL,
00151 32* C60H BASE MATERIALS LABOR INDIRECT RANGE /%
00151 33* COX60H COST COSTS COSTS COSTS COSTS COSTS
00151 34* C UNLOADING AND STORAGE OF FISH
00152 35* TONSA = TONS*2000./8.33
00153 36* GALLON = TONSA/(24.*60.)
00154 37* GALS = 1.3* GALLON
00155 38* SUMHP=0.
00156 39* IA(65,1) =0.
00157 40* IA(65,2) =1.0
00160 41* AA(65,17)= GALS*30.
00161 42* NUM = TONS/500 + 1
00162 43* DO 143 I=1,NUM
00165 44* SUMHP=SUMHP+(I.*AA(65,17)*.001*1.5)
00166 45* CALL PMPREC
00170 46* IA(65,2)=0.
00171 47* IF(TONSA.LT.30000.) G=(30000./(24.*60.))*15.
00173 48* IF(TONSA.GE.30000.) G=(450000./(24.*60.))*15.
00175 49* IF(TONS.LE.150.) AA(70,1A)=36.
00177 50* IF(TONS.GE.150.) AA(70,1A)=48.
00201 51* AA(70,17)=100.
00202 52* CALL BELT
00203 53* HP= TONS*.00124 + 13.6
00204 54* SUMHP= SUMHP + HP
00205 55* AA(40,17)= 30.0* TONS
00206 56* IA(40,1) = 0
00207 57* IA(40,2) = 2
00210 58* CALL STORAG
00211 59* IA(40,2)= 0
00212 60* AA(85,17)= 0.5* TONS* 3.0
00213 61* IA(85,1) = 30
00214 62* CALL REFRIG
00215 63* IA(7,1) = 1
00215 64*
00215 65*
00215 66*
00215 67*
00216 68* AA(7,17)=3.*TONS*2000.*1.69/62.4
00217 69* CALL SILO
00220 70* COST(1)=1.19
00221 71* IF(TONS.GE.300) COST(1)=1.88
00223 72* COST(5)=COST(1)
00224 73* PRINT 4249, COST(1), COST(5)
00230 74* COSTA(1)=COSTA(1)+COST(1)
00231 74* COSTA(5)=COSTA(5)+COST(5)

```

Table I.- Continued.

00232	75*	4249	FORMAT(/25H BRINE MAKE-UP+SALT STOR., 10X ,15H	,10H
00232	76*	1	,F10.3,3,X,F10.3)	
00232	77*	C	PUMP FOR BRINE MAKE-UP (BRONZF)	
00232	78*	C		
00232	79*	C		
00233	80*		IA(66,1)=1	
00234	81*		AA(66,17)=TONS*3.*2000./(24.*60.*62.4)*.69*7.75	
00235	82*		CALL PMPCNT	
00236	83*		IA(66,1)=0	
00237	84*		HP=.001*AA(66,17)	
00240	85*		SUMHP=SUMHP+HP	
00240	86*	C		
00240	87*	C	PUMP FOR WATER INTO BRINE MAKE-UP	
00240	88*	C		
00241	89*		AA(66,17)=AA(66,17)*.917	
00242	90*		IA(66,1)=0	
00243	91*		CALL PMPCNT	
00244	92*		HP=.001*AA(66,17)	
00245	93*		SUMHP=SUMHP+HP	
00246	94*		TONSG= TONS/24.	
00247	95*		AA(71,18)= TONSG	
00250	96*		AA(71,17)= 20.	
00251	97*		CALL BUCKET	
00252	98*		HP= TONS* 0.00106	
00253	99*		SUMHP=HP+SUMHP	
00253	100*	C	FISH GRINDING AND EXTRACTION	
00254	101*		IF(IPTION(1).EQ.1) GO TO 100	
00254	102*	C		
00254	103*	C	URY DERONING	
00256	104*		AA(11,17)= TONS* 2000./24.	
00257	105*		BB(2) = 3.0	
00260	106*		CALL PULVER	
00261	107*	1120	FORMAT(/44H	THE DRY DEBONING OPTION IS APPROPRIATE)
00262	108*	1110	FORMAT(/44H	THE WET DEBONING OPTION IS APPROPRIATE)
00263	109*		ZA1=0.	
00264	110*		ZA3=1.	
00265	111*		GO TO 101	
00266	112*	130	CONTINUE	
00266	113*	C		
00266	114*	C	WET DEBONING	
00266	115*	C		
00267	116*		ZA1=0.04	
00270	117*		ZA3=0.	
00271	118*		NR= 1	
00272	119*		NA= (TONS/75.) + 1.	
00273	120*		IF(NA.GT.3) NB = 2	
00275	121*		IF(NA.GT.3) NA = (TONS/150.)+1.	
00277	122*		DO 113 J = 1,NA	
00302	123*		L00PS = L00PS + 1	
00303	124*		COST(1) = 22.*BB(1)	
00304	125*		IF(NB.EQ.2) COST(1) = 40.* BB(1)	
00306	126*		HP=10.	
00307	127*		IF(NB.EQ.2) HP= 20.	
00311	128*		SUMHP = SUMHP +	HP
00312	129*		COST(2)= COST(1)* .25	
00313	130*		COST(3)= COST(1)* .25	
00314	131*		COST(4)= COST(1)* .4	

Table I.--Continued.

```

00315 132* COST(5)= COST(1)+ COST(2) + COST(3) +COST(4)
00316 133* COST(6)= .1 * COST(1)
00317 134* DO 114 K=1,7
00322 135* COSTA(K)= COSTA(K) + COST(K)
00324 136* STONE =75.
00325 137* IF (NB,EO.2) STON = 150.
00327 138* PRINT 1113 ,STON,(COST(K),K=1,6)
00336 139* LOOPS=L00PS + 1
00337 140* CONTINUE
00341 141* CONTINUE
00342 142* ZA2=1. -ZA1
00342 143*
C
00342 144* C EXTRACTION VESSELS MATERIAL RALATICE
00342 145* C 1=OIL 2=PROTEIN 3=ASH 4=WATER 5= IPA
C
00342 146*
00343 147* STM(1,1)=TONS*RB(3n)*ZA2
00344 148* STM(1,2)=.17*STM(1,1)
00345 149* STM(1,3)=.29*STM(1,2)
00346 150* STM(1,4)=.5*STM(1,3)
00347 151* STM(1,5)=.25*STM(1,4)
00350 152* STM(2,1)=TONS*7A2*RB(31)
00351 153* STM(2,2)=.8*STM(2,1)
00352 154* STM(2,3)=.98*STM(2,2)
00353 155* STM(2,4)=1.0*STM(2,3)
00354 156* STM(2,5)=.99*STM(2,4)
00355 157* STM(3,1)=TONS*7A3*RB(32)
00356 158* STM(3,2)=.81*STM(3,1)
00357 159* STM(3,3)=.98*STM(3,2)
00360 160* STM(3,4)=.99*STM(3,3)
00361 161* STM(3,5)=.99*STM(3,4)
00362 162* STM(4,1)=TONS*7A2*RB(33)
00363 163* STM(4,2)=.29*STM(4,1)
00364 164* STM(4,3)=.56*STM(4,2)
00365 165* STM(4,4)=.60*STM(4,3)
00366 166* STM(4,5)=.12*STM(4,4)
00367 167* STM(5,1)=0.
00370 168* STM(5,2)=TONS/50.*1.5
00371 169* STM(5,3)=1.29*STM(5,2)
00372 170* STM(5,4)=1.87*STM(5,3)
00373 171* STM(5,5)=1.84*STM(5,4)
00374 172* STRM(1,5)=0.
00375 173* STRM(2,5)=0.
00376 174* STRM(3,5)=0.
00377 175* STRM(5,5)=TONS*2.
00400 176* STRM(4,5)=0.
00401 177* DO 122 I=4,1,-1
00404 178* DO 122 J=1,5
00407 179* STRM(J,I)= STRM(J,I+1) -STM(J,I+1) +STM(J,I)
00412 180* DO 123
00415 181* * STRM(I)=0.
00415 182* * STRM(I)=0.
00417 183* DO 123 J= 1,5
00422 184* STRM(I)=STMM(I) + STM(J,I)
00423 185* STRM(I)=STPM(I)+ STRM(J,I)
00424 186* CONTINUE
00424 187* C
00424 188* C EXTRACTION VESSEL

```

Table I.-- Continued.

```

00424 189*
00427 190*
00430 191*
00431 192*
00431 193*
00432 194*
00433 195*
00434 196*
00435 197*
00436 198*
00437 199*
00440 200*
00441 201*
00442 202*
00443 203*
00444 204*
00445 205*
00446 206*
00450 207*
00452 208*
00455 209*
00456 210*
00457 211*
00460 212*
00461 213*
00462 214*
00464 215*
00466 216*
00466 217*
00466 218*
00466 219*
00467 220*
00470 221*
00471 222*
00472 223*
00473 224*
00474 225*
00475 226*
00476 227*
00500 228*
00501 229*
00503 230*
00505 231*
00506 232*
00507 233*
00510 234*
00511 235*
00512 236*
00513 237*
00514 238*
00516 239*
00521 240*
00522 241*
00523 242*
00524 243*
00525 244*
00526 245*

C
TONSA=(TONS*ZA1) + (TONS*BB(32)*ZA2*(1,-ZA3))
TONSU= TONS-TONSA
SLMXTK= 875.* TONSR / 50.
MIX TANK
GALS= 875.* TONS/50.
AA(73,17)= GALS*.005
IA(66,1)= 2
IA(73,5)= 2
AA(40,17)= GALS
AA(40,18)= 3.2
AA(41,12)=3.2
IA(40,1)= 1
CALL STORAG
GAA= STRMM(1)*2000./(24.*60.)
GAA=GAA/8.33
AA(66,17)=GAA*10.
IF(GAA.GT.125.) IP= (GAA/125.) + 1
IF(GAA.LE.125.) IP=1
DO 40 I0=1,IP
HP=(AA(66,17)*.001)
SUMHP=HP+SUMHP
CALL PMPCNT
AA(66,17)=(STRMM(1)+STRMM(2))*2000.*30./(24.*60.*8.33)
SUMHP=.001*AA(66,17)+SUMHP
40 CALL PMPCNT
IF (GALS. GT. 10000.) AA(73,17)=50.
CALL AGIT0R

C
REACTOR VESSFLS

C
AA(51,17)=TONS*60./50.
IP=(AA(51,17)/144.) +2.
AA(51,17) =IP
VES= TONS* 30.
AA(49,17) = VES
VSS= TONS*16.
IR=1
IF(VES.GT.10000.) IP= (VES/10000.) + 1.
IRR=1
IF(VSS.GT.10000.) TRP= (VSS/10000.)*1.
IF(VES.GT.10000.) TANK= 800.* TONS/50.
AA(40,18) = 3.2
AA(41,18) = 3.2
AA(40,17) = TANK
CALL STORAG
SAG= STRMM(2)*2000./(24.*8.33*60.)
IP=1
IF(SAG.GT.12500.) IP =(SAG/12500.) + 1.
DO 93 IU=1,IP
XIP = IP
AA(66,17) = (SAG/XIP)* 24.
CALL PMPCNT
CALL PMPCNT
HP=.001*AA(66,17)
SUMHP=SUMHP+HP

```


Table I.- Continued.

```

00527 246* SUMHP=SUMHP+HP
00530 247* 93 CONTINUE
00532 248* IF(VLESS.GT,10000.,) VFESS=10000.
00534 249* DO 41 I = 1,IR
00537 250* LOOPS = LOOPS + 3
00540 251* AA(49,17)=VES
00541 252* CALL REACTR
00542 253* CALL SCREEN
00543 254* AA(73,17)=.005*VFS
00544 255* IF(AA(73,17).LT.2.) AA(73,17)=2.
00546 256* IA(73,5)=2
00547 257* CALL AGITOR
00550 258* SUMHP=SUMHP + 2.5
00551 259* XIR= IR
00552 260* SUMHP = SUMHP + AA(73,17)
00553 261* AA(66,17) = TONS*2000./(24.*8.33*XIR) *(22./60.)
00554 262* CALL PMPCNT
00555 263* ABC= AA(66,17)/22.
00556 264* IF(ABC.LE.2.) HP=2.
00560 265* IF(ABC.GT.2.) HP=ARC
00562 266* SUMHP= HP + SUMHP
00563 267* IA(17,5)=5
00564 268* DX= SORT(TONS/50.1) * 8.
00565 269* AA(17,17) = 6
00566 270* AA(17,18) = DX
00567 271* CALL SCREWPR
00570 272* 41 CONTINUE
00572 273* DO 42 J= 1,IPR
00575 274* LOOPS = LOOPS + 9
00576 275* DO 42 I = 1,3
00601 276* XIRR=IRR
00602 277* SUMHP=SUMHP + 2.5
00603 278* AA(66,17) = TONS*2000./(24.*8.33*XIRR) *(22./60.)
00604 279* CALL PMPCNT
00605 280* ABC= AA(66,17)/22.
00606 281* IF(ABC.GT.2.) HP=ARC
00610 282* IF(ABC.LE.2.) HP=2.
00612 283* SUMHP= HP + SUMHP
00613 284* AA(49,17)=VFESS
00614 285* CALL REACTR
00615 286* CALL SCREEN
00616 287* AA(73,17)=.005*VFS
00617 288* IF(AA(73,17).LT.2.) AA(73,17)=2.
00621 289* IA(73,5)=2
00622 290* SUMHP = SUMHP + AA(73,17)
00623 291* CALL AGITOR
00624 292* DX= SORT(TONS/50.1) * 8.
00625 293* AA(17,18) = DX
00626 294* AA(17,17) = 6.
00627 295* IA(17,5)=5
00630 296* CALL SCREWPR
00631 297* 42 CONTINUE
00631 298* C PUMPS IN THE EXTRACTION PROCESS
00631 299* C PUMPS FOR S-1
00634 300* AA(66,17)=STMM(2)*30.*2000./(24.*60.*8.33)
00635 301* CALL PMPCNT
00636 302* SUMHP=.001*AA(66,17)+SUMHP

```

Table I.--Continued.

```

00636 303* C PUMP FOR S-2
00637 304* AA(66,17)=STMM(3)*2000.*30./(24.*60.*8.33)
00640 305* CALL PMPCNT
00641 306* SUMHP=.001*AA(66,17)+SUMHP
00641 307* C PUMP FOR S-3
00642 308* AA(66,17)=STMM(4)*2000.*30./(24.*60.*8.33)
00643 309* CALL PMPCNT
00644 310* SUMHP=.001*AA(66,17)+SUMHP
00644 311* C PUMP FOR M-3
00645 312* AA(66,17)=STMM(3)*2000.*30./(24.*60.*8.33)
00646 313* CALL PMPCNT
00647 314* SUMHP=.001*AA(66,17)+SUMHP
00647 315* C PUMP FOR SOLIDS INTO DRYER
00650 316* AA(66,17)=STMM(5)*2000.*30./(24.*60.*8.33)
00651 317* CALL PMPCNT
00652 318* SUMHP=.001*AA(66,17)+SUMHP
00652 319* C PUMP FOR M-4
00653 320* AA(66,17)=STMM(4)*2000.*30./(24.*60.*8.33)
00654 321* CALL PMPCNT
00655 322* SUMHP=.001*AA(66,17)+SUMHP
00655 323* C PUMP FOR SOLVENT
00656 324* AA(66,17)=TONS*2.*2000.*30./(24.*60.*8.33)
00657 325* CALL PMPCNT
00660 326* SUMHP=.001*AA(66,17)+SUMHP
00660 327* C REFLUX CONDENSFR
00660 328*
00661 329* FF = 25.* TONS/ 50.
00662 330* AA(67,17) = FF
00663 331* CALL HEATEX
00663 332* C
00663 333* C STEAM REQUIREMENTS
00664 334* STEAM2= TONS* 20./50.
00665 335* STEAM3= TONS* 20./50.
00666 336* STEAM4= TONS* 20./50.
00667 337* STEAM1= TONS* 35./50.
00670 338* STEAM= STEAM1+STEAM2+STEAM3+STEAM4
00670 339* C
00670 340* C SOLIDS FROM THE EXTRACTION VFSSEL
00670 341* C
00671 342* TASC= STMM(5)/2.
00672 343* TASB=STM(1,5)+STM(2,5)+STM(3,5)+.05*STM(4,5)+STM(5,5)*.126*.05+STM
1(5,5)*.0001*.874
00673 344* TASC=.95*.126*STM(5,5)+.95*STM(4,5)
00674 345* TASD=STM(5,5)*.874*.9999
00675 347* STEAM6= (TASC + (1.0*TASD)) * 2000. /24.
00676 348* STEAM= STEAM6 + 5TFAM
00676 349* C DRYERS
00677 350* AA(21,17) = 3.8* 16.* TASC/24.
00700 351* IA(21,5) = 6
00701 352* BB(2) = .9
00702 353* CALL DRYERR
00703 354* BR(2)=1.0
00704 355* AA(21,17)=AA(21,17)
00705 356* IA(21,5) = 7
00706 357* CALL DRYERR
00707 358* AA(17,18)=6.
00710 359* AA(17,17)=6.

```

Table I.-- Continued.

```

00711 360* IA(17,5)=1
00712 361* CALL SCREWR
00713 362* BB(2)=1.
00714 363* IA(21,5)=7
00715 364* AA(21,17)=AA(21,17)
00716 365* CALL DRYERR
00717 366* AA(21,17)=AA(21,17)
00720 367* IA(21,5) = 8
00721 368* BB(2)=1.0
00722 369* CALL DRYERR
00723 370* AA(17,18)=6
00724 371* AA(17,17)=6
00725 372* IA(17,5)=1
00726 373* CALL SCREWR
00727 374* L00PS = L00PS + 2
00730 375* L00PS = L00PS + 2
00731 376* AA(17,18) = 6.
00732 377* AA(17,17) = 20.
00733 378* IA(17,5) = 1
00734 379* CALL SCREWR
00735 380* ZAT= .96
00736 381* IF(IPTION(2).NF,1) ZAT=1.
00740 382* ZAR=1.-ZAT
00741 383* IF(IPTION(2).NE,1.AND.IPTION(2).NE,2) GO TO 300
00743 384* AA(18,17) =(TASR/ 8.)
00744 385* CALL HAMMER
00745 386* HP = (TASB *2000.*75./(8. * 700.))
00746 387* HP = HP/3.
00747 388* SUMHP=SUMHP+HP
00750 389* IF(IPTION(2).EQ,1) GO TO 44
00752 391* DRY DEBONING OPTI0N
00753 392* PRDCTA=((STM(2,5)*ZAT) + (STM(3,5)*7AR))/.95
00754 393* AA(75,17)=PRDCTA*2000./(25.*24.*60.)
00755 394* CALL BAGGMA
00756 395* XAA=AA(75,17)
00757 396* AA(75,17)=PRDCTR*2000./(25.*24.*60.)
00760 397* CALL BAGGMA
00761 398* AA(75,17)=AA(75,17) +XAA
00762 399* AA(75,17)=AA(75,17)*24.*60.
00763 400* GO TO 49
00764 401* CONTINUE
00765 402* AA(18,17)=TASR/8.
00766 403* CALL HAMMER
00767 404* HP=(TASB*2000.*75./(8.*700.))
00770 405* HP=HP/3.
00771 406* SUMHP=SUMHP+HP
00772 407* PRDCTA=((STM(2,5)+STM(3,5))/.95)
00773 408* AA(75,17)=PRDCTA*2000./(25.*24.*60.)
00774 409* CALL BAGGMA
00775 410* AA(75,17)=AA(75,17)*24.*60.
00776 411* GO TO 49
00777 412* CONTINUE
00777 413* 44 CONTINUE
01000 414* C WET DEBONING OPTI0N
01001 415* AA(75,17) =(STM(2,5)*ZAT) + (STM(3,5)*7AR)/.95
01002 416* AA(75,17) = AA(75,17)* 2000./(24.*60.*100.) * 4.

```

Table I.-- Continued.

```

01003 417* CALL BAGGMA
01004 418* AABAG=AA(75,17)
01005 419* 40 CONTINUE
01005 420* C MIXING TANK SECTION
01005 421* C
01005 422* C
01006 423* SA = STRMM(1)*.001*70.
01007 424* IA(40,1) = 1
01010 425* IA(40,2) = 1
01011 426* AA(40,17) = SA
01012 427* CALL STORAG
01013 428* IA(40,2) = 0
01014 429* LOPPS = LOPPS + 2
01015 430* ACID = STRMM(1)*.001
01016 431* IA(66,1) = 2
01017 432* AA(66,17) = 30.*ACID *2000./(8.33*60.*24.* 1.8)
01020 433* CALL PMPCNT
01021 434* GAL = STRMM(1) * 2000. / (8.33 )
01022 435* HP = .001*AA(66,17)
01023 436* SUMHP = HP + SUMHP
01024 437* AA(40,17) = GAL *.01
01025 438* AA(66,17) = GAL *30./(24.*60.)
01026 439* IA(66,1) = 0
01027 440* IA(40,1) = 2
01030 441* HP = .001*AA(66,17)
01031 442* SUMHP = SUMHP + HP
01032 443* SUMHP = SUMHP+HP
01033 444* CALL PMPCNT
01034 445* CALL STORAG
01035 446* CALL PMPCNT
01035 447* C CENTRIFUGE SECTION
01035 448* C
01035 449* C
01036 450* SAA = STRMM(1)*1.001
01037 451* HOP = SAA*2000.*.01/(24.*8.33 )
01040 452* NUM = (HOP/20.) + 1.
01041 453* HP = NUM* 20
01042 454* SUMHP = HP + SUMHP
01043 455* DO 45 I = 1,NUM
01046 456* AA(54,17) = 20.
01047 457* CALL CNTFGE
01050 458* CONTINUE
01052 459* SAB = STRM(1,1)*1.1
01053 460* HP = SAB*.025*2000./(8.33*24.)
01054 461* N2 = (HP/20.) + 1.
01055 462* HP = N2*20
01056 463* SUMHP = SUMHP+HP
01056 464* C PUMP BETWEEN CENTRIFUGES
01057 465* AA(66,17) = SAA*2000.*30./(24.*60.*8.33)
01060 466* CALL PMPCNT
01061 467* SUMHP = .001*AA(66,17) + SUMHP
01062 468* DO 46 I = 1,N2
01065 469* AA(52,17) = 20.
01066 470* CALL SHARP
01066 471* C FISH OIL STORAGE TANK (15 DAYS)
01066 472* C
01066 473* C

```

Table I.--Continued.

```

01067 474* AA(90,5)=STRM(1,1)
01070 475* AA(40,17)=AA(90,5)*2000.*15./7.75
01071 476* IA(40,1)=1
01072 477* CALL STORAG
01073 478* AA(66,17)=AA(40,17)*30./(24.*15.*60.)
01074 479* CALL PMPCNT
01075 480* SUMHP=.001*AA(66,17)+SUMHP
01076 481* 46 CONTINUE
01076 482* C
01076 483* C MISCELLA TANK (M=1)
01076 484* C
01100 485* SBC=STRM(1)-(.5*STRM(1,1))
01101 486* AA(40,18)=3.*2
01102 487* AA(41,18)=3.*2
01103 488* AA(40,17)=SBC*2000./(24.*8.33)
01104 489* IA(40,1)=1
01105 490* CALL STORAG
01106 491* AA(66,17)=30.*(AA(40,17)/60.)
01107 492* IA(66,1)=0
01110 493* CALL PMPCNT
01111 494* CALL PMPCNT
01112 495* HP=.001*AA(66,17)
01113 496* SUMHP=SUMHP+HP
01114 497* SUMHP=SUMHP+HP
01114 498* C PREHEATER FOR DISTILLATION COLUMN
01114 499* C
01115 500* SRC=STRM(1)-(.5*STRM(1,1))
01116 501* STEAMQ=SBC*2000./24.*1
01117 502* STEAM = STEAM + STEAMQ
01120 503* FTE STEAM*.1
01121 504* AA(67,17) = FT
01122 505* CALL HEATEX
01122 506* C
01122 507* C DISTILLATION COLUMN (MATERIAL BALANCE)
01122 508* C
01123 509* STOP(1)=STRM(5,1)*.9987*.874
01124 510* STOP(2) =STOP(1) *.1445
01125 511* SBOT(1)=STRM(5,1)*.00113*.874
01126 512* SBOT(2)=STRM(4,1)+.125*STRM(5,1)-STOP(2)
01127 513* SBOT(3) = STRM(1,1)*.5
01130 514* SBOTT= SBOT(1) + SBOT(2) + SBOT(3)
01130 515* C
01130 516* C CENTRIFUGE
01130 517* C
01131 518* AA(66,17)=30.*SBOTT*2000./(60.*24.*8.33)
01132 519* IA(66,1) = 0
01133 520* CALL PMPCNT
01134 521* SUMHP=.001*AA(66,17)+SUMHP
01135 522* HP= SBOTT*2000./(24.*8.33
01136 523* N3=(HP/20.) + 1
01137 524* HP= 20* N3
01140 525* SUMHP= HP + SUMHP
01141 526* DO 47 I=1,N3
01144 527* AA(54,17) = 20.
01145 528* CALL CNTFGE
01146 529* 47 CONTINUE
01150 530* LOOPS = LOOPS + (NIM+ N2 + N3)

```

Table I.-- Continued.

```

01150 C 531*
01150 C 532*
01150 C 533*
01151 C 534*
01152 C 535*
01153 C 536*
01154 C 537*
01155 C 538*
01156 C 539*
01157 C 540*
01160 C 541*
01161 C 542*
01162 C 543*
01163 C 544*
01164 C 545*
01165 C 546*
01166 C 547*
01167 C 548*
01171 C 549*
01172 C 550*
01173 C 551*
01174 C 552*
01175 C 553*
01176 C 554*
01177 C 555*
01200 C 556*
01201 C 557*
01202 C 558*
01203 C 559*
01204 C 560*
01205 C 561*
01206 C 562*
01207 C 563*
01210 C 564*
01211 C 565*
01212 C 566*
01213 C 567*
01214 C 568*
01214 C 569*
01215 C 570*
01216 C 571*
01217 C 572*
01220 C 573*
01221 C 574*
01222 C 575*
01223 C 576*
01223 C 577*
01223 C 578*
01223 C 579*
01224 C 580*
01225 C 581*
01226 C 582*
01227 C 583*
01230 C 584*
01232 C 585*
01234 C 586*
01235 C 587*

C U I S T I L L A T I O N   C O L U M N
STFAMR=TONS*10709./50.*(STRM(5,5)/(TONS*2.))
AA(67,17)=.1*STEAMP
CALL HEATEX
STFAM = STFAM + STFAMP
TANKA = TONS* 100. /50.
IA(40,1)= I
AA(40,17)=TANKA*2000./ (24.*8.33)
CALL STORAG
AA(66,17)=(TANKA-(.01*STRM(5,5))*(2000.*30.)/(24.*60.*8.33)
CALL PMPCNT
SUMHP=.001*AA(66,17)+SUMHP
WIDTH = 4. * SORT(TONS/75.)
I = WIDTH/2.
WIDTH = 2 * I
IF (WIDTH.LT.4.001) WIDTH = 4.
AA(43,18) = 24.
AA(43,20)=WIDTH
AA(43,17)= 54.
AA(43,1) = .4
IA(42,4)=2
IA(42,2)=1
IA(42,3)=1
AA(42,18)=WIDTH
AA(42,19)=54
CALL VESSEL
CALL COLUMN
LOOPS = LOOPS + 5
WASTE=.01*STRM(5,5)
AA(40,17)=(WASTE*2000./8.33*15.)
IA(40,1) = 0
CALL STORAG
AA(66,17)=AA(40,17)*30./(24.*60.*15.)
CALL PMPCNT
SUMHP=.001*AA(66,17)+SUMHP
LOOPS = LOOPS + 1
CONDENSER(DISTILLATION COLUMN)
WATER=669.*TONS/50.*(STRM(5,5)/(TONS*2.))
AA(67,17)=WATER*8.33*60.*.01
CALL HEATEX
AA(66,17)=(TANKA/60.)*30.
CALL PMPCNT
HP = 2. *(TONS /75.)
SUMHP=SUMHP+HP
C F I S H   S O L U A B L E S
SBOT=SBOT(2) + STRM(2,1)
SBOQT=STRM(2,1)*2.
HWAT=SBOT-SBQQT
FORMAT(/50H FISH SOLUABLES ARE MORE THAN 50 PERCENT PROTEIN
IF (HWAT.GE.0.) GO TO 51
PRINT ,3006
AA(90,4)=SBOT
GO TO 52

```

Table I.--Continued.

01236	588*	51	CONTINUE
01236	589*	C	
01236	590*	C	WATER SOLUBLES HOI D TANK (1 HR)
01236	591*	C	
01237	592*	C	AA(40,17)=SBQT*2000./(24.*8.4)*1.
01240	593*		IA(40,1)=1
01241	594*		CALL STORAG
01242	595*		IA(40,1)=0
01243	596*		IA(66,1)=0
01244	597*		AA(66,17)=30.*AA(40,17)/60.
01245	598*		CALL PMPCNT
01246	599*		HP=.001*AA(66,17)
01247	600*		SUMHP=SUMHP+HP
01250	601*		AA(99,4)=SBQT
01251	602*		TONA=SBQT*2000./24.
01252	603*		AA(33,17)=TONA/20.
01253	604*		CALL EVPHOR
01254	605*		CALL EVPHOR
01255	606*		CALL EVPHOR
01256	607*		SAQT= STRM(2,1)/.3
01257	608*		IF(SAQT.GE.SBOT) SAQT=SRQT
01261	609*		AA(33,17)=SAQT*2000./(24.*25.)
01262	610*		CALL EVPHOR
01263	611*		STEAM=STEAM+(H*AT*2000./24.)
01264	612*		IA(66,1)=0
01265	613*		AA(66,17)=30.*STRM(2,1)*2.*2000./(10.*60.*24.)
01266	614*		CALL PMPCNT
01267	615*		HP=.001*AA(66,17)
01270	616*		SUMHP=SUMHP+HP
01270	617*	C	
01270	618*	C	ACID MIX TANK
01270	619*	C	
01271	620*		AA(40,17)=STRM(2,1)*2.*2000./(10.*1.)*.01
01272	621*		IA(40,1)=2
01273	622*		CALL STORAG
01274	623*		IA(40,1)=0
01274	624*	C	
01274	625*	C	STORAGE OF FISH SOLUBLES (15 DAYS)
01274	626*	C	
01275	627*		IA(66,1)=0
01276	628*		AA(66,17)=30.*AA(40,17)/(40.*24.)
01277	629*		CALL PMPCNT
01301	630*		HP=.001*AA(66,17)
01302	631*		SUMHP=SUMHP+HP
01302	632*		IA(40,1)=2
01303	633*		AA(40,17)=STRM(2,1)*2.*2000./(10.)*15.
01304	634*		CALL STORAG
01305	635*		IA(40,1)=0
01306	636*		CONTINUE
01307	637*	52	CONTINUE
01311	638*		IF(IPTION(2).NE.1) GO TO 48
01311	639*	C	IF (IPTION(2).EQ.1) L00PS = 100PS + 1
01313	640*		AA(91,2) = TONS - STMM(1)
01313	641*	C	PUMP FOR BONE FEED TO DRYFR
01314	642*		AA(66,17)=AA(91,2)*2000.*30./(24.*60.*8.33)
01315	643*		CALL PMPCNT
01316	644*		SUMHP=.001*AA(66,17)+SUMHP

Table I.--Continued.

01317	645*	IA(21,5)=3
01320	646*	AA(21,7)=AA(91,2)*3.8*2.73,
01321	647*	STEAMW=AA(91,2)*2000./24.
01322	648*	STEAM=STEAM + STEAMW
01323	649*	CALL DRYERR
01324	650*	AA(90,3)=(100NS*(RB(31)+RB(32)+RB(30)) - STM(1,1) - STM(2,1)
01324	651*	- STM(3,1)) * 1.1
01324	652*	C HAMMER MILL FOR WET DEBONING OPTION
01325	653*	AA(18,17) = AA(90,3) / 24.
01326	654*	CALL HAMMER
01327	655*	AA(75,17)=AA(90,3)*2000.*.04/(24.*60.)
01330	656*	CALL BAGGMA
01331	657*	AA(75,17)=(AA(75,17) +AARAG) *24.*60.
01332	658*	48 CONTINUE
01332	659*	C BOILER
01333	660*	AA(27,18) =150.
01334	661*	AA(27,17)=STEAM
01335	662*	CALL BOILER
01336	663*	IA(40,1)=2
01337	664*	AA(40,17)=STFAM*1000.*24./(8.33*140000.)*15.
01340	665*	CALL STORAG
01341	666*	IA(66,1)=0
01342	667*	AA(66,17)=30.*AA(40,17)/(40.*15.*24.)
01343	668*	CALL PMPCNT
01344	669*	HP=.001*AA(66,17)
01345	670*	SUMHP=SUMHP+HP
01345	671*	CONTROL LOOP
01346	672*	XLOOPS = L00PS
01347	673*	COST(1) = X100PS*AA(100,1)
01350	674*	COST(5) = COST(5)
01351	675*	COSTA(1) = COSTA(1) + COST(1)
01352	676*	COSTA(5) = COSTA(5) + COST(5)
01353	677*	PRINT 1021, COST(1),COST(5)
01353	678*	C FORK LIFT
01357	679*	1021 FORMAT(/25H CONTROL INSTRUMENTATION ,35X,F10.3,30X,F10.3)
01360	680*	COST(1) = AA(100,20)
01361	681*	COST(5) = COST(1)
01362	682*	COSTA(1) = COSTA(1) + COST(1)
01363	683*	COSTA(5) = COSTA(5) + COST(5)
01364	684*	PRINT 1022, COST(1),COST(5)
01370	685*	AA(8,17) = TONS
01371	686*	CALL CONDEN
01372	687*	1022 FORMAT(/ 25H PAYLOADER , 10X,25X,F10.3,30X,F10.3)
01372	688*	C BOILER WATER TREATMENT
01372	689*	C
01372	690*	COST(5)=1.000
01373	691*	COST(1)=COST(5)
01374	692*	PRINT 4242,COST(1),COST(5)
01375	693*	4242 FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H ,10H
01401	694*	1 ,F10.3,30X,F10.3)
01401	695*	COSTA(1)=COSTA(1)+COST(1)
01402	696*	COSTA(5)=COSTA(5)+COST(5)
01403	697*	C SEA WATER PUMPS
01403	698*	C
01403	699*	AA(90,10)=WATER*60.+4.*STFAM
01404	701*	

Table I.-- Continued.

01405	702*	AA(66,17)=AA(90,10)*1.2/60.	
01406	703*	IA(66,1)=1	
01407	704*	IA(66,4)=2	
01410	705*	CALL PMPCNT	
01411	706*	IA(66,1)=0	
01412	707*	IA(66,4)=0	
01413	708*	HP=.001*AA(66,17)	
01414	709*	SUMHP=SUMHP+HP	
01414	710*	C CARBON ADSORBER	
01414	711*	C	
01414	712*	COST(1)=2.000	
01415	713*	COST(5)=COST(1)	
01416	714*	PRINT 4243,COST(1),COST(5)	
01417	715*	COSTA(1)=COSTA(1)+COST(1)	
01423	716*	COSTA(5)=COSTA(5)+COST(5)	
01424	717*	FORMAT(/25H CARBON ADSORBER	
01425	718*	1 ,F10.3,30X,F10.3)	
01425	719*	10X ,15H ,10H	
01425	720*	C VENT CONDENSER	
01425	721*	C	
01425	722*	AA(67,17)=20	
01426	723*	IA(67,1)=1	
01427	724*	IA(67,4)=4	
01430	725*	CALL HEATEX	
01431	726*	IA(67,1)=0	
01432	727*	IA(67,4)=0	
01433	728*	CALL SCALE	
01434	729*	CALL SCALE	
01435	730*	CALL SCALE	
01436	731*	CALL SCALE	
01437	732*	CALL SCALE	
01440	733*	PRINT 1041,(COSTA(J),J=1,6)	
01446	734*	FORMAT(/25H TOTAL COSTS	
01447	735*	AA(90,2) = SUMHP*.7457 * 24.	
01450	736*	AA(100,10)= COSTA(5)	
01451	737*	AA(90,1) = STFAM*1000.*24./140000.	
01451	738*	MATERIAL BALANCE	
01452	739*	IF(IPTION(2).EQ.2) AA(90,3)=PPDCTR	
01454	740*	AA(90,7) = PRDCTA	
01455	741*	AA(90,18)=WASTE	
01456	742*	AA(90,19)=ACID	
01457	743*	CALL WATER(TONS)	
01460	744*	FISH = TONS*2000./24.	
01461	745*	PRINT 1003 , FISH	
01464	746*	FORMAT(/7X27H FISH TO EXTRACTION VESSELS,F8.0,7H LB/HR)	
01465	747*	YYA=STEAM1	
01466	748*	PRINT 1201,YYA	
01471	749*	FORMAT(/BX,15H STFAM(STIRRED VESSEL 1)	
01472	750*	YYB=STEAM2	
01473	751*	PRINT 1202,YYB	
01476	752*	FORMAT(/BX,15H STFAM(STIRRED VESSEL 2)	
01477	753*	YYC= STEAM3	
01500	754*	PRINT 1203,YYC	
01503	755*	FORMAT(/BX,15H STFAM(STIRRED VESSEL 3)	
01504	756*	YYD= STEAM4	
01505	757*	PRINT 1204,YYD	
01510	758*	FORMAT(/BX,15H STFAM(STIRRED VESSEL 4)	

Table I.-- Continued.

01511	759*	YYE = STEAM0	
01512	760*	PRINT 1205,YYF	
01515	761*	FORMAT(/8X,35H STFA,(PREHEATEP-DISTILLATION)	,F8.0,7H LR/HR)
01516	762*	YYG= STEAMR	
01517	763*	PRINT 1206,YYG	
01522	764*	FORMAT(/8X,35H STFA,(PCBOILER)	,F8.0,7H LR/HR)
01523	765*	YYH = STEAMK	
01524	766*	PRINT 1207,YYH	
01527	767*	FORMAT(/8X,35H STFA,(ROTARY DRYER FPC)	,F8.0,7H LR/HR)
01530	768*	YYI= STEAMW	
01531	769*	PRINT 1208,YYT	
01534	770*	FORMAT(/8X,35H STEAM(ROTARY DRYER BONE MEAL)	,F8.0,7H LR/HR)
01535	771*	YYJ=(STEAM*4.)	
01546	772*	PRINT 1209,YYJ	
01541	773*	YYK= WATER	
01542	774*	PRINT 1210,YYK	
01545	775*	FORMAT(/8X,35H COOLING WATER DISTILLATION COND.	,F8.0,8H GAL/MIN)
01546	776*	FORMAT(/8X,35H COOLING WATER CONDENSER	,F8.0,8H GAL/HR)
01547	777*	YYL= STEAM	
01550	778*	PRINT 1211,YYL	
01553	779*	FORMAT(/8X,35H TOTAL STEAM	,F8.0,7H LR/HR)
01554	780*	YYM=(STEAM*4.)+WATER*60.1*8.33	
01555	781*	PRINT 1212,YYM	
01560	782*	FORMAT(/8X,35H TOTAL WATER	,F8.0,7H LR/HR)
01561	783*	PRINT 1213	
01563	784*	FORMAT(/40X, 9H STAFAM 1.7X,9H STREAM 2.7X,9H STREAM 3.7X,9H STR	
01563	785*	CEAM 4.7X,9H STREAM 5,/))	
01564	786*	PRINT 1214,(STRM(1,K),K=1,5)	
01572	787*	PRINT 1215,(STRM(2,K),K=1,5)	
01600	788*	PRINT 1216,(STRM(3,K),K=1,5)	
01606	789*	PRINT 1217,(STRM(4,K),K=1,5)	
01614	790*	PRINT 1218,(STRM(5,K),K=1,5)	
01622	791*	PRINT 1219,(STM (1,K),K=1,5)	
01630	792*	PRINT 1220,(STM (2,K),K=1,5)	
01636	793*	PRINT 1221,(STM (3,K),K=1,5)	
01644	794*	PRINT 1222,(STM (4,K),K=1,5)	
01652	795*	PRINT 1223,(STM (5,K),K=1,5)	
01660	796*	FORMAT(/10X,20H RAFFINATE OIL	,10X,4(F10.3, RX),F10.3)
01661	797*	FORMAT(/10X,20H RAFFINATE ASH	,10X,4(F10.3, RX),F10.3)
01662	798*	FORMAT(/10X,20H RAFFINATE WATER	,10X,4(F10.3, RX),F10.3)
01663	799*	FORMAT(/10X,20H RAFFINATE ALCOHOL	,10X,4(F10.3, RX),F10.3)
01664	800*	FORMAT(/10X,20H RAFFINATE OIL	,10X,4(F10.3, RX),F10.3)
01665	801*	FORMAT(/10X,20H EXTRACT ASH	,10X,4(F10.3, RX),F10.3)
01666	802*	FORMAT(/10X,20H EXTRACT OIL	,10X,4(F10.3, RX),F10.3)
01667	803*	FORMAT(/10X,20H EXTRACT WATER	,10X,4(F10.3, RX),F10.3)
01670	804*	FORMAT(/10X,20H EXTRACT ALCOHOL	,10X,4(F10.3, RX),F10.3)
01671	805*	FORMAT(/10X,20H EXTRACT	
01672	806*	XXA= STMM(5)* 2000./24.	
01673	807*	PRINT 1224, XVA	
01676	808*	FORMAT(/8X,35H FLOW FROM EXTRACTION VESSEL 4	,F8.0,7H LR/HR)
01677	809*	XXB= STMM(1)* 2000./24.	
01700	810*	FORMAT(/8X,35H FLOW FROM EXTRACTION VESSEL 1	,F8.0,7H LR/HR)
01701	811*	PRINT 1225, XXB	
01704	812*	XXC = (SAW-(.5*STMM(1,1)))*2000./24.	
01705	813*	PRINT 1226,XXC	
01710	814*	FORMAT(/8X,35H AMIENS STREAM(CENTRIFUGF)	,F8.0,7H LR/HR)
01711	815*	XXD=(STOP(1)+STOP(2))*2000./24.	

Table I.-- Continued.

```

01712 816* PRINT 1227,XXH
01715 817* FORMAT(/8X,15H TOPS FROM DISTILLATION COLUMN ,F8.0,7H LR/HR )
01716 818* XXE= SBOOT*2000./24.
01717 819* PRINT 1228,XXE
01722 820* FORMAT(/8X,15H BOTTOMS FROM DISTILLATION COLUMN ,F8.0,7H LR/HR )
01723 821* XXF=(.5*STRM(1,1)*2000./24.)
01724 822* PRINT 1229,XXF
01727 823* FORMAT(/8X,15H OIL FROM SECOND CENTRIFUGE ,F8.0,7H LR/HR )
01730 824* XXG= AA(90,5)*2000./24.
01731 825* PRINT 1230,XXG
01734 826* FORMAT(/8X,15H FISH OIL PRODUCT ,F8.0,7H LR/HR )
01735 827* XXH=AA(90,3)*2000./24.
01736 828* FORMAT(/8X,15H FISH PROTEIN CONCENTRATE ,F8.0,7H LR/HR )
01737 829* XXI=AA(90,7)*2000./24.
01740 830* PRINT 1232,XXH
01743 831* PRINT 1231,XXI
01746 832* FORMAT(/8X,15H BONE MEAL CONCENTRATE ,F8.0,7H LR/HR )
01747 833* AA(95,1) = STRM(1,2) * 2.
01750 834* XXJ = AA(95,1)* 2000./24.
01751 835* PRINT 1233,XXJ
01754 836* FORMAT(/8X,15H FISH SOLUBLES ,F8.0,7H LR/HR )
01755 837* IXX=(14.0*(TONS/50.)***.31) + 0.5
01756 838* AA(90,8)=IXX**8
01757 839* AA(90,9)=(YYJ+YYK**6.)*24.
01760 840* AA(90,13) = AA(90,13) + (AA(90,3)+AA(90,7)+AA(90,20)+AA(90,4))
01761 841* RETURN
01762 842* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S PRESCK,PRESCK
FOR 59A-07/12-11:04 (1.)

SUBROUTINE PRESCK ENTRY POINT 002401

STORAGE USED: CODE(1) 002445; DATA(0) 001006; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 PMPREC
0006 BELT
0007 STORAG
0010 REFRIG
0011 SILO
0012 PMPCNT
0013 BUCKET
0014 DRYERR
0015 SCREWR
0016 SCREEN
0017 REACTR
0020 AGITOR
0021 HAMMER
0022 RAGGMA
0023 FVPELM
0024 EVPSPR
0025 SHARP
0026 HOLLER
0027 CONDEN
0030 SCALE
0031 WATER
0032 NRDC\$
0033 NI02\$
0034 NPRT\$
0035 NI01\$
0036 NEXP6\$
0037 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	00046	1000F	0000	00005	1001F	0000	00073	1002F	0000	000260	1003F	0000	000271	1004F
0000	00302	1005F	0000	00033	1006F	0000	000324	1007F	0000	000335	1008F	0000	000370	1009F
0001	00722	101L	0000	00040	1010F	0000	000412	1011F	0000	000423	1012F	0000	000434	1013F
0000	00045	1014F	0000	00045	1015F	0000	000467	1016F	0000	000346	1017F	0000	000500	1018F
0000	00051	1019F	0001	00075	102L	0000	000522	1020F	0000	000533	1021F	0000	000544	1022F
0000	00055	1023F	0001	00104	103L	0000	000566	1030F	0000	000577	1031F	0000	000610	1032F
0000	00035	1033F	0000	00025	1041F	0000	000215	1050F	0000	000233	1051F	0001	000024	1066
0000	00034	111F	0001	00003	1146	0001	000036	1226	0000	000106	2000F	0001	000152	2016
0000	00012	3000F	0001	00046	3056	0001	000177	4242F	0000	000161	4249F	0000	000036	5000F

Table I.--Continued.

0001 001450 6006 0001 001525 622G 0001 002001 727G 0001 002027 742G 0003 R 000000 AA
 0003 R 004704 BB 0000 R 000030 C00L 0004 R 000000 COST 0000 R 000007 COSTA
 0000 R 000027 FISH 0000 R 000006 G 0000 R 000002 GALLON 0000 R 000003 GALS
 0000 I 000000 I 0003 I 003720 IA 0000 000771 TNJPS 0000 I 000017 INST 0000 I 000032 IXX
 0000 I 000026 J 0000 I 000010 LOOPC 0000 I 000012 NA 0000 I 000005 NUM 0000 R 000022 PROD
 0000 R 000033 PXX 0000 R 000021 SLD5 0000 R 000031 STEAM 0000 R 000004 SUMHP 0000 R 000001 TONSA
 0000 R 000011 TONSG 0000 R 000020 VOLD 0000 R 000016 VOLT 0000 R 000023 WATER
 0000 R 000015 XL10D 0000 R 000025 XLOOPS 0000 R 000013 XNA

00101 1* SUBROUTINE PRESCK(TONS)
 00103 2* COMMON/BLOCK1/AA(100,20),TA(100,5),BB(100)
 00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
 00105 4* DO 1 I=1,7
 00110 5* COST(I) =0.0
 00111 6* COSTA(I)=0.0
 00113 7* DO 2 I=1,20
 00116 8* AA(90,I) =0.0
 00121 9* DO 10 I=30,33
 00124 11* BB(I) = BB(I)*0.01
 00126 12* READ 111 ,BB(40),BR(41),BR(42),BR(43),BR(44)
 00135 13* FORMAT(5E12.5)
 00136 14* PRINT 5000
 00140 15* FORMAT(/BX36H ANTIOXIDANT PRICE AND EFFECTIVENESS)
 00141 16* PRINT 1001,RR(44),RR(43)
 00145 17* PRINT 1000
 00147 18* FORMAT(/BX31H ENZYME PRICE AND EFFECTIVENESS)
 00150 19* PRINT 1001,RR(41),BR(40)
 00154 20* FORMAT(/BX8H PRICE =,F5.2,1PH DOLLARS/LR,FA.3,3RH LR REQUIRED PF
 00154 21* CR 100 LB OF PRESS CAKE)
 00155 22* IF(RB(42) .GT. 0.0) PRINT 1002,RR(42)
 00161 23* IF(RB(42) .GT. 0.0) PRINT 1002,RR(42)
 00161 24* CSTE)
 00162 25* PRINT 2000
 00164 26* FORMAT(1H1/5RH DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL
 00164 27* CLARS))
 00165 28* PRINT 3000
 00167 29* FORMAT (/21RH EQUIPMENT TYPE,10X10H CAPACITY,12X0H MATERIAL,
 00167 30* C60H BASE MATERIALS LABCR INDIRECT MODULE RANGE ,/A
 00167 31* C0X60H COST COSTS COSTS COST + OR -)
 00167 32* C
 00167 33* C UNLOADING AND STORAGE OF FISH
 00167 34* C
 00170 35* TONSA=TONS*2000./A.*33
 00171 36* GALLONE TONCA/(24.*60.)
 00172 37* GALS =GALLON*1.3
 00173 38* SUNHPE = 0.
 00174 39* IA(65,1) = 0
 00175 40* IA(65,2) = 1.0
 00176 41* AA(65,17)= GALS*30.
 00177 42* NUM = TONS/500 + 1
 00200 43* DO 143 I=1,NUM
 00203 44* CALL PMPREC
 00205 45* IA(65,2) = 0.0

Table I.--Continued.

```

00206          SUMHP= SUMHP +(AA(65,17)*.001*1.5)
00207          SUMHP= SUMHP +(AA(65,17)*.001*1.5)
00210          IF(TONSA*LT.30000.) G=(30000./(24.*60.))*15.
00212          IF(TONSA*GE.30000.) G=(450000./(24.*60.))*15.
00214          IF(TONS.LE.150.) AA(70,18)= 36.
00216          IF(TONS.GT.150.) AA(70,18)= 48.
00220          AA(70,17)=100.
00221          CALL BELT
00222          HP = TONS*0.00124 +13.6
00223          SUMHP = HP + SUMHP
00224          AA(40,17)=30.0*TONS
00225          IA(40,1)=0.0
00226          IA(40,2)=2
00227          CALL STORAG
00230          IA(40,2)=0
00231          AA(85,17)=0.5*TONS**3.0
00232          IA(85,1) =30
00233          CALL REFRIG
00234          SUMHP = SUMHP + 4.7*AA(85,17)
00235          IA(7,1)=1
00236
00237          C
00238          C FISH STORAGE FOR 3 DAYS
00239          C
00240          AA(7,17)=3.*TONS*2000.*1.69/62.4
00241          CALL SILO
00242          COST(1)=1.19
00243          IF(TONS*GE.300) COST(1)=1.88
00244          COST(5)=COST(1)
00245          PRINT 4249, COST(1), COST(5)
00246          COSTA(1)=COSTA(1)+COST(1)
00247          COSTA(5)=COSTA(5)+COST(5)
00248          FORMAT(/25H BRINE MAKE-UP+SALT STOR., 10X ,15H
00249          1 ,F10.3,3nX,F10.3)
00250          C
00251          C PUMP FOR BRINE MAKE-UP (BRONZE)
00252          C
00253          IA(66,1)=1
00254          AA(66,17)=TONS*3.*2000./(24.*60.*62.4)*.69*7.75
00255          CALL PMPCNT
00256          IA(66,1)=0
00257          HP=.0010*AA(66,17)
00258          SUMHP=SUMHP+HP
00259          C
00260          C PUMP FOR WATER INTO BRINE MAKE-UP
00261          C
00262          AA(66,17)=AA(66,17)*.917
00263          IA(66,1)=0
00264          CALL PMPCNT
00265          HP=.0010*AA(66,17)
00266          SUMHP=SUMHP+HP
00267          L00PS=0.0
00268          L00PS=L00PS+3.
00269          TONSG=TONS/24.
00270          AA(71,18)= TONSG
00271          CALL BUCKET
00272          HP = TONS*0.00106
00273          101*
00274          102*

```

Table I.--Continued.

00275	103*	SUMHP = HP + SUMHP
00275	104*	
00275	105*	C FISH COOKERS AND SCREW PRESS
00275	106*	
00276	107*	
00277	108*	AA(91,16) = 0.2*TONS
00300	109*	AA(91,10)=TONS+AA(01,16)
00302	110*	IF (TONS .GT. 450) NA=(TONS/250) +1.
00304	111*	IF (TONS .LF. 450) NA=(TONS/100) +1.
00307	112*	DO 3 I=1,NA
00310	113*	BB(2)=2.1
00311	114*	XNA = NA
00312	115*	IA(21,5)=4
00313	116*	AA(21,17)=TONS/XNA
00314	117*	CALL DRYERR
00315	118*	C PUMP TO PRESS
00316	119*	AA(66,17)=AA(91,10)*30.*2000./(24.*8.33*60.)
00317	120*	IA(66,1)=0
00320	121*	CALL PMPCNT
00321	122*	HP=.001*AA(66,17)
00322	123*	SUMHP=HP+SUMHP
00323	124*	IA(17,5)=3
00325	125*	BR(2)=2.6
00327	126*	IF (TONS .GT. 450) AA(17,17)= 21.
00331	127*	IF (TONS .GT. 450) AA(17,18)= 16.
00333	128*	IF (TONS .LE. 450) AA(17,18)= 12.
00334	129*	IF (TONS .LE. 450) AA(17,17)= 15.
00336	130*	CALL SCREW
00340	131*	IF (TONS .GT. 450) AA(51,17)= 10.0
00341	132*	IF (TONS .LE. 450) AA(51,17)= 4.0
00343	133*	CALL SCREEN
00344	134*	3 CONTINUE
00345	135*	DRYSLD=(.8*BR(32)+.94*BR(31))*TONS
00345	136*	XLIQDE=(BB(30)+BB(33))+.06*RR(31)+.2*BB(32))*TONS+AA(91,16)
00345	137*	AA(90,16)=2.86*DRYSLD
00345	138*	
00345	139*	C FISH DIGESTION AND SCREENING
00345	140*	
00345	141*	C SCREW CONVEYOR
00345	142*	
00346	143*	AA(17,18)=6
00347	144*	AA(17,17)=20
00350	145*	IA(17,5)=1
00351	146*	CALL SCREW
00352	147*	AA(90,18)=AA(91,10)-AA(90,16)
00353	148*	AA(90,5)=TONS*RB(30)*(397./500.)
00354	149*	AA(7,17)=27.4*AA(90,16)*50.
00355	150*	CALL SILO
00356	151*	AA(91,17)=AA(91,10)-AA(90,16)-AA(90,5)
00356	152*	C PUMP FOR WATER AND SLUDGE
00357	153*	AA(66,17)=AA(91,17)*2000.*30./(24.*60.*8.33)
00360	154*	IA(66,1)=0
00361	155*	CALL PMPCNT
00362	156*	HP=.001*AA(66,17)
00363	157*	SUMHP=HP+SUMHP
00364	158*	AA(90,15)=AA(90,16)*.0084
00365	159*	AA(90,13)=(BR(30)+BR(31)+BR(32))*TONS*.0001

Table I.-- Continued.

```

00366 160* AA(90,17)=TONS*0.022
00367 161* AA(90,12)=AA(90,16)*RB(40)/100.0
00370 162* AA(91,1)=AA(90,16)+AA(90,17)+AA(90,15)+AA(90,12)+AA(91,17)+AA(90,1
00370 163* C3)
00371 164* VOLT=AA(91,1)*2000/(R*.33*4.8)
00372 165* AA(51,2) = 2.0
00373 166* AA(51,17) = 2.0
00374 167* AA(49,17)=VOLT/3
00375 168* IF(AA(49,17) .LT. 10000) AA(73,17) = AA(49,17)*0.005
00377 169* IF(AA(49,17) .LT. 10000) GO TO 101
00401 170* IF( AA(49,17) .GT. 10000) AA(73,17) = 50.
00403 171* IF(AA(49,17) .GT. 10000) AA(49,17)=10000
00405 172* CALL REACTR
101 CALL AGITR
00406 173* CALL SCREEN
00407 174* CALL REACTR
00410 175* CALL REACTR
00411 176* CALL AGITR
00412 177* CALL SCREEN
00413 178* CALL REACTR
00414 179* CALL AGITR
00415 180* CALL SCREEN
00416 181* INST = 3
00417 182* HP = 3*AA(73,17)
00420 183* SUMHP = HP + SUMHP
00421 184* VOLD =VOLT -AA(49,17)*3
102 IF(VOLD .LT. 500) GO TO 103
00422 185* IF(VOLD .LT. 10000) AA(49,17)=VOLD
00424 186* IF(AA(49,17) .LT. 10000) AA(73,17) = AA(49,17)*0.005
00430 187* IF(VOLD .GT. 10000) AA(49,17)=10000
00432 188* IF( AA(49,17) .GT. 10000) AA(73,17) = 50.
00434 190* CALL REACTR
00435 191* CALL AGITR
00436 192* CALL SCREEN
00437 193* INST = INST + 1
00440 194* VOLD = VOLD -AA(49,17)
00441 195* HP = AA(73,17)
00442 196* SUMHP = HP + SUMHP
00443 197* GO TO 102
00444 198* C
00444 199* C
103 CONTINUE
00444 200* C
00444 201* C
C BONE FEED STREAM
00445 202* BB(2)=1.
00446 203* SLD5=((155./667.)*RB(31))+((68./145.)*RB(32))+((103./500.)*(14./10
00446 204* C3.)*BB(30))*TONS+(20./112.)*(AA(90,12)+AA(90,13)+AA(90,15)+AA(90
00446 205* 1,17))*(68./145.)
00447 206* AA(91,2)=(340./137.)*SLD5
C SCREW CONVEYOR
00447 207* C
00447 208* C
00447 209* C
00450 210* AA(17,18)=6
00451 211* AA(17,17)=20
00452 212* IA(17,5)=1
00453 213* CALL SCREW
00454 214* IA(21,5)=3
00455 215* AA(21,17)=AA(91,2)*2.5
00456 216* CALL DRYERR

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Table I.-- Continued.

00457	217*	AA(90,3)=1.05*SLIDS
00460	218*	AA(91,12)=AA(91,2)-AA(90,3)
00460	219*	
00460	220*	C BAGGING MACHINE AND HAMMER MILL FOR BONE FEED
00460	221*	C
00461	222*	AA(75,17)=AA(90,3)*2000./(24.*60.*25.)
00462	223*	IA(75,2)=0
00463	224*	IA(75,1)=0
00464	225*	AA(18,17)=AA(90,3)/24.
00465	226*	CALL HAMMER
00466	227*	CALL BAGGMA
00467	228*	AA(75,5)=AA(75,17)
00467	229*	C
00467	230*	C DIGESTED SOLIDS STREAM
00467	231*	C
00467	232*	
00470	233*	AA(91,3) =AA(91,1)-AA(91,2)
00471	234*	AA(40,17) = AA(91,3)*2000./(8.33*24)
00472	235*	IA(40,1)=1
00473	236*	CALL STORAG
00474	237*	IA(40,1) = 0
00474	238*	C PUMPS BEFORE AND AFTER HOLD TANK
00475	239*	
00476	240*	IA(66,1)=0
00477	241*	AA(66,17)=AA(40,17)*30./60.
00500	242*	CALL PMPCNT
00501	243*	SUMHP=SUMHP+2.*.001*AA(66,17)
00502	244*	AA(91,6)=AA(91,3)
00503	245*	PROD=((612./667.)*BR(31))+((89./103.)*(103./500.)*BB(30))+((77./1
00503	246*	C45.)*BB(32))*TONS+((20./112.)*(AA(90,12)+AA(90,13)+AA(90,15)+AA(9
00503	247*	10,17))*77./145.)
00504	248*	WATER=AA(91,3)-PRON
00505	249*	WATEVP =WATER-PRON
00506	250*	HP=0.01*AA(91,3)*2000./(8.33*24.)
00507	251*	SUMHP=HP+SUMHP
00510	252*	AA(91,13)=WATEVP
00511	253*	AA(31,17)=AA(91,13)*2000./(24.*25)
00512	254*	CALL EVPFLM
00512	255*	
00512	256*	C HOLD TANK FOR DIGESTED SOLIDS
00512	257*	C
00513	258*	AA(91,7)=2.*PRON
00514	259*	AA(40,17)=AA(91,7)*2000./(8.33*24.)
00515	260*	IA(40,1)=0
00516	261*	CALL STORAG
00516	262*	C PUMP AFTER WIPED FILM EVAPORATOR
00517	263*	
00520	264*	AA(66,17)=AA(40,17)*30./60
00521	265*	IA(66,1)=0
00522	266*	CALL PMPCNT
00522	267*	HP=.001*AA(66,17)
00523	268*	SUMHP=HP+SUMHP
00524	269*	AA(90,6)=AA(91,7)*RB(42)*.01
00524	269*	C PUMP BEFORE CANNING MACHINE
00525	270*	
00526	271*	AA(66,17)=AA(90,6)*2000.*30./(8.33*24.*60.)
00530	272*	IF(BB(42).GT.0.0) CALL PMPCNT
00531	273*	HP=.001*AA(66,17)
		SUMHP=HP+SUMHP

Table I.--Continued.

```

00532 274* AA(75,17)=AA(90,6)*2000.0/(8.33*24.0*60.0*5.0)
00533 275* IA(75,1)=1.0
00534 276* IA(75,2)=2.0
00535 277* IF(BB(42).GT.0.0) CALL RAGGMA
00537 278* AA(75,4)=AA(75,17)
00540 279* IA(75,1)=0.0
00541 280* IA(75,2)=0.0
00542 281* AA(75,4)=AA(75,4)*60.*24.
00543 282* AA(91,9)=AA(91,7)-AA(90,6)
00544 283* AA(90,7)=AA(91,9)/(2.*.95)
00544 284* C PUMP BEFORE SPRAY DRYER
00545 285* AA(66,17)=AA(90,7)*2000.*30./(8.33*60.*24.)
00546 286* IA(66,1)=0
00547 287* CALL PMPCNT
00550 288* HP=.001*AA(66,17)
00551 289* SUMHP=HP+SUMHP
00552 290* AA(91,14)=AA(91,9)-AA(90,7)
00553 291* AA(30,17)=AA(91,14)*2000.0/24.0
00554 292* CALL EVSPR
00555 293* AA(75,17)=(AA(75,17)+AA(75,5))*60.*24.
00556 294* IF(BB(42).LT.100) CALL RAGGMA
00560 295* AA(75,17)=AA(75,17)*60.*24.
00560 296* C FISH OIL STREAM
00560 297* C
00560 298* AA(40,17)=AA(90,18)*2000/(8.33*24)
00561 299* IA(40,1)=N
00562 300* CALL STORAG
00563 301* CALLS AFTER SCREFN AND BFFORE CENTRIFUGE
00564 302* AA(66,17)=AA(40,17)*30./60.
00565 303* IA(66,1)=0
00566 304* CALL PMPCNT
00567 305* CALL PMPCNT
00570 306* HP=.001*AA(66,17)
00571 307* SUMHP=HP+SUMHP
00572 308* SUMHP=HP+SUMHP
00573 309* SUMHP=HP+SUMHP
00574 310* AA(91,4)=1.1*AA(90,5)
00575 311* HP=0.01*AA(90,18)*2000.0/(8.33*24.0)
00576 312* SUMHP=HP+SUMHP
00577 313* NUM=HP/20.+1
00602 314* DO 40 I=1,NUM
00602 315* AA(52,17)=20.
00603 316* CALL SHARP
00605 317* AA(40,17)=AA(91,4)*2000/(8.33*24)
00606 318* CALL STORAG
00606 319* C PUMP BEFORE AND AFTER HOLD TANK
00607 320* AA(66,17)=AA(40,17)*30./60.
00610 321* IA(66,1)=0
00611 322* CALL PMPCNT
00612 323* CALL PMPCNT
00613 324* HP=.001*AA(66,17)
00614 325* SUMHP=HP+SUMHP
00615 326* SUMHP=HP+SUMHP
00616 327* HP=0.025*AA(91,4)*2000.0/(8.33*24.0)
00617 328* SUMHP=HP+SUMHP
00620 329* NUM=HP/20.+1
00621 330* DO 30 I=1,NUM

```

Table I.--Continued.

00624	331*	AA(52,17) =20.0	
00625	332*	CALL SHARP	
00625	333*	C	
00625	334*	C FISH OIL STORAGE (15 DAYS)	
00625	335*	C	
00627	336*	AA(40,17)=AA(90,5)*2000./A.33*15.	
00630	337*	IA(40,1) =0.0	
00631	338*	CALL STORAG	
00632	339*	AA(66,17)=AA(90,5)*.001*2000.0/(8.33*24*60)	
00633	340*	SUMHP= SUMHP+(AA(66,17)*0.001)	
00634	341*	IA(66,1) =1	
00635	342*	CALL PMPCNT	
00635	343*	C	
00635	344*	C SUMMATION OF STEAM,WATER AND ELECTRICITY	
00635	345*	C	
00636	346*	AA(91,15)=(AA(91,11)+AA(91,12)+AA(91,13)+AA(91,14))*1.05 +	
00636	347*	C 1.05*(AA(91,16) +AA(91,18) +AA(91,19))	
00637	348*	AA(27,17)=AA(91,15)*2000.0/24	
00640	349*	CALL BOILER	
00640	350*	C	
00640	351*	C BOILER WATER TREATMENT	
00640	352*	C	
00641	353*	COST(1)=1.000	
00643	355*	COST(5)=COST(1)	
00647	356*	PRINT 4242,COST(1),COST(5)	
00647	357*	FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H	
00650	358*	1 ,F10.3,30X,F10.3)	
00651	359*	COSTA(5)=COSTA(5)+COST(5)	
00651	361*	COSTA(1)=COSTA(1)+COST(1)	
00651	362*	C	
00652	363*	C FUEL OIL STORAGE (15 DAYS)	
00652	364*	C	
00654	365*	IA(40,1)=2	
00655	366*	AA(40,17)=AA(27,17)/A.33*24.*.0012*15.	
00655	367*	CALL STORAG	
00656	368*	AA(66,17)=30.*AA(40,17)/(15.*60.)	
00657	369*	CALL PMPCNT	
00660	370*	HP=.0010*AA(66,17)	
00661	371*	SUMHP=SUMHP+HP	
00661	372*	C	
00661	373*	C SEA WATER PUMPS	
00662	374*	C	
00663	375*	AA(90,10)=4.*8.33*(AA(91,13)+AA(91,14)+AA(91,18)+AA(91,19))*1.2	
00664	376*	AA(66,17)=AA(90,10)*2000.0/(8.33*24*60*0.066)	
00664	377*	IA(66,1)=1	
00665	378*	IA(66,4)=2	
00666	379*	CALL PMPCNT	
00667	380*	IA(66,4)=0	
00670	381*	IA(66,1)=0	
00671	382*	SUMHP = SUMHP+(AA(66,17)*.001*1.5)	
00672	383*	AA(90,9) =1.1*(3*TONS+AA(90,15)/.15 +0.1*AA(91,4)+AA(91,16))	
00673	384*	XLOOPS=L00PS+18.*3.*INST+NA	
00675	385*	COST(1)=XLOOPS *AA(100,1)	
00676	386*	COST(5)=COST(1)	
00677	387*	COSTA(1) = COSTA(1) + COST(1)	
		COSTA(5)=COSTA(5) + COST(5)	

Table I.--Continued.

00700	388*	PRINT 1050 COST(1),COST(5)	
00704	389*	1050 FORMAT(/ 25H CONTROL INSTRUMENTATION , 10X ,15H	,10H
00704	390*	1 F10.3,30X,F10.3)	
00705	391*	AA(8,17) = TONS	
00706	392*	CALL CONDEN	
00707	393*	AA(72,17) = 1R.	
00710	394*	CALL SCALE	
00711	395*	CALL SCALE	
00712	396*	CALL SCALE	
00713	397*	CALL SCALE	
00714	398*	COST(1)=AA(100,2)	
00715	399*	COST(5)=COST(1)	
00716	400*	COSTA(1)=COST(1)	+ COSTA(1)
00717	401*	COSTA(5)=COSTA(5) + COST(5)	
00720	402*	PRINT 1051, COST(1),COST(5)	
00724	403*	1051 FORMAT(/ 25H PAYLOADER AND FORK LIFT , 10X ,15H	,10H
00724	404*	1 F10.3,30X,F10.3)	
00725	405*	PRINT 1041,(COSTA(J),J=1,6)	
00733	406*	1041 FORMAT(/25H TOTAL COSTS	,35X6F10.3)
00734	407*	COSTA(7)=0.02*COSTA(1)	
00735	408*	AA(100,10)=COSTA(5)	
00735	409*		
00735	410*		
00735	411*		
00736	412*		
00737	413*	AA(90,2) = SIMP* .7457 * 24.	
00740	414*	AA(90,10)=AA(90,10)*2000./(24.*8.33)	
00741	415*	CALL WATER(TONS)	
00744	416*	DO 50 I=1,20	
00745	417*	AA(90,I)=AA(90,I)*2000/24	
00747	418*	AA(91,I)=AA(91,I)*2000/24	
00750	419*	FISH=TONS*2000/24	
00753	420*	PRINT 1003,FISH	
00754	421*	1003 FORMAT(/8X26H FISH FEED TO COOKERS	,F8.0,7H LB/HR)
00757	422*	PRINT 1004,AA(91,16)	
00760	423*	1004 FORMAT(/8X26H COOKERS STFAM	,F8.0,7H LB/HR)
00763	424*	PRINT 1005,AA(90,16)	
00764	425*	1005 FORMAT(/8X26H PREFCS CAKE TO DIGESTERS	,F8.0,7H LB/HR)
00767	426*	PRINT 1006,AA(91,17)	
00770	427*	1006 FORMAT(/8X26H FISH SOL. TO DIGESTERS	,F8.0,7H LB/HR)
00773	428*	PRINT 1007,AA(90,12)	
00774	429*	1007 FORMAT(/8X26H ENZYMF TO DIGESTERS	,F8.2,7H LB/HR)
00777	430*	PRINT 1008,AA(90,15)	
01003	431*	1008 FORMAT(/8X26H CAOH TO DIGESTERS	,F8.2,7H LB/HR)
01004	432*	PRINT 1017,AA(90,13)	
01007	433*	1017 FORMAT(/8X26H ANTI-OXIDANT TO DIGESTERS	,F8.2,7H LB/HR)
01010	434*	PRINT 1033,AA(90,17)	
01010	435*	1033 FORMAT(/8X26H 5N NAOH TO DIGESTERS	,F8.2,7H LB/HR)
01013	436*	PRINT 1009,AA(91,2)	
01014	437*	1009 FORMAT(/8X26H FEED TO ROTARY DRYER	,F8.0,7H LB/HR)
01017	438*	PRINT 1010,AA(91,12)	
01020	439*	1010 FORMAT(/8X26H ROTARY DRYER STEAM	,F8.0,7H LB/HR)
01023	440*	PRINT 1011,AA(90,3)	
01024	441*	1011 FORMAT(/8X26H BONF FEED PRODUCT	,F8.0,7H LB/HR)
01027	442*	PRINT 1012,AA(91,3)	
01030	443*	1012 FORMAT(/8X26H DIGESTER LIQUOR	,F8.0,7H LB/HR)
01033	444*	PRINT 1013,AA(91,6)	
		1013 FORMAT(/8X26H FEED TO FILM EVAPORATOR	,F8.0,7H LB/HR)

Table I.--Continued.

01034	445*	PRINT 1014,AA(91,13)	
01037	446*	FORMAT(/8X26H FILM EVAPORATOR STEAM	,F8.0,7H LB/HR)
01040	447*	COOL =AA(91,13)*4	
01041	448*	PRINT 1015,COOL	
01044	449*	FORMAT(/8X26H FILM EVAPORATOR COOLING	,F8.0,7H.6AL/HR)
01045	450*	PRINT 1016,AA(91,7)	
01050	451*	FORMAT(/8X26H FISH PASTE	,F8.0,7H LB/HR)
01051	452*	AA(90,13)=0.05*AA(91,7)*0.01	
01052	453*	PRINT 1018,AA(90,6)	
01055	454*	FORMAT(/8X26H PACKAGED AS FISH PASTE	,F8.0,7H LB/HR)
01056	455*	PRINT 1019,AA(91,9)	
01061	456*	FORMAT(/8X26H FEED TO SPRAY EVAPORATOR	,F8.0,7H LB/HR)
01062	457*	PRINT 1020,AA(91,14)	
01065	458*	FORMAT(/8X26H SPRAY EVAPORATOR STEAM	,F8.0,7H LB/HR)
01066	459*	COOL=4*AA(91,14)	
01067	460*	PRINT 1021,COOL	
01072	461*	FORMAT(/8X26H SPRAY EVAP. COOLING	,F8.0,7H GAL/HR)
01073	462*	PRINT 1022,AA(90,7)	
01076	463*	FORMAT(/8X26H DRY CONCENTRATE	,F8.0,7H LB/HR)
01077	464*	PRINT 1023,AA(90,5)	
01102	465*	FORMAT(/8X26H FISH OIL	,F8.0,7H LB/HR)
01103	466*	STEAM=AA(27,17)-AA(91,12)-AA(91,13)-AA(91,14)-AA(91,18)-AA(91,19)	
01103	467*	C-AA(91,16)	
01104	468*	PRINT 1030,STEAM	
01107	469*	FORMAT(/8X26H MISCELLANEOUS STEAM	,F8.0,7H LB/HR)
01110	470*	AA(90,9)=AA(90,9)/8.33	
01111	471*	PRINT 1031,AA(90,9)	
01114	472*	FORMAT(/8X26H CITY WATER	,F8.0,7H GAL/HR)
01115	473*	AA(90,10)=AA(90,10)*24./2000.	
01116	474*	PRINT 1032,AA(90,10)	
01121	475*	FORMAT(/8X26H PROCESS WATER	,F8.0,7H GAL/HR)
01122	476*	AA(90,11) = AA(27,17)*24*0.0112	
01123	477*	AA(90,2) = SUMHP* .7457 * 24.	
01124	478*	AA(90,3) = AA(90,3)*24/2000	
01125	479*	AA(90,5) = AA(90,5)*24/2000	
01126	480*	AA(90,6) = AA(90,6)*24/2000	
01127	481*	AA(90,7) = AA(90,7)*24/2000	
01130	482*	IXX =(14.0*(TONS/50.0)**.31) +0.5	
01131	483*	PXX =IXX	
01132	484*	AA(90,8) =IXX*8.0	
01133	485*	AA(90,9) =AA(90,9)*24	
01134	486*	AA(90,12)=AA(90,12)*24	
01135	487*	AA(90,13)=AA(90,13)*24	
01136	488*	AA(90,15)=AA(90,15)*24	
01137	489*	AA(90,17)=AA(90,17)*24	
01140	490*	RETURN	
01141	491*	END	

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S HOPPER,HOPPER
FOR S9A-07/12-11:04 (0,)

SUBROUTINE HOPPER ENTRY POINT 00007*

STORAGE USED: CODE(1) 000100; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NIO1\$
0010 NIO2\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 0000003 116G 0001 000055 125G 0003 R 004704 BB
0004 R 000000 COST 0004 R 0000007 COSTA 0000 I 000001 I 0003 R 000000 IA
0000 I 000000 IX 0000 I 0000002 J 0000 I 000001 I 0000 000021 INJPS

SUBROUTINE HOPPER

```

00101 1* SUBROUTINE HOPPER
00103 2* IX = 6
00104 3* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105 4* COMMON /BLOCK2/ COST(7),COSTA(7)
00106 5* COST(1) = COST(1)*AA(IX,18)
00107 6* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO I =1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H CONICAL HOPPER ,F10.3,15H CUBIC FT. ,10H
00131 16* C SST ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPIATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S SILO,SILO
FOR S9A-07/12-11:04 (0,)

SUBROUTINE SILO ENTRY POINT 000116

STORAGE USED: CODE(1) 000122; DATA(0) 000050; BLANK COMMON(2) 000000

COMMON RLOCKS:

0003 RLOCK1 005050
0004 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NIO1\$
0010 NIO2\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00003 1000F 0000 000020 1001F 0001 000047 120G 0001 000063 130G 0001 000101 140G
0003 R 000000 AA 0003 R 004704 BB 0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I
0003 I 003720 IA 0000 000000 INJPS 0000 I 000002 J

```

00101 1* SUBROUTINE SILO
00103 2* IX=7
00104 3* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105 4* COMMON/BLOCK2/ COST(7),COSTA(7)
00106 5* IF(IA(7,1) .EQ.1) AA(7,11)=0.20
00110 6* COST(1)= BB(1)* AA(7,7)*AA(7,17)**AA(7,8)
00111 7* COST(1)= .001* COST(1)
00112 8* COST(2) = COST(1)* AA(7,11)
00113 9* COST(3)= COST(1)* AA(7,12)
00114 10* COST(4)= COST(1)* AA(7,13)
00115 11* COST(5)= COST(1)+ COST(2)+COST(3) +COST(4)
00116 12* COST(6)= COST(1)*AA(7,15)
00117 13* DO 1 I =1,7
00122 14* 1 COSTA(I)=COST(I) + COSTA(I)
00124 15* IF(IA(7,1) .EQ.0) PRINT 1000 ,AA(7,17),(COST(I),I=1,6)
00134 16* IF(IA(7,1) .EQ.1) PRINT 1001,AA(7,17),(COST(J),J=1,6)
00144 17* 1000 FORMAT(/ 25H STORAGE BIN
00144 18* 1 STEEL ,6F10.3)
00145 19* 1001 FORMAT(/25H REDWOOD STORAGE BIN ,F10.0,15H CUBIC FEET ,10H
00145 20* CREDWOOD ,6F10.3 )
00146 21* RETURN
00147 22* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S CONDEN,CONDEN
FOR S9A-07/12-11:04 (0,)

SUBROUTINE CONDEN ENTRY POINT 000065

STORAGE USED: CODE(1) 000071; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000006 116G 0001 000050 125G
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 T
0000 I 000000 IX 0000 T 000002 J

0003 R 004704 BB
0000 000022 INJPS

0003 R 000000 AA
0003 003720 IA

```

00101 1* SUBROUTINE CONDEN
00103 2* IX=8
00104 3* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105 4* COMMON/BLOCK2/ COST(7),COSTA(7)
00106 5* COST(1)=BB(1)*AA(R,7)*AA(R,17)**AA(R,R)
00107 6* COST(1) = COST(1)*0.001
00110 7* COST(2) = COST(1) * AA(8,11)
00111 8* COST(3) = COST(1) * AA(8,12)
00112 9* COST(4) = COST(1) * AA(8,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(1)*AA(R,15)
00115 12* DO 1 I= 1,7
00120 13* 1 COSTA(I) = COSTA(I) + COST(I)
00122 14* PRINT 1000, AA(8,17), (COST(J),J=1,6)
00131 15* 1000 FORMAT(/ 25H SCRUBFRS ,F10.3,15H TONS PROCESSED,10H
00131 16* 1 STEEL ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S PULVER,PULVER
FOR S9A-07/12-11:04 (0,)

SUBROUTINE PULVER ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000043 1176 0001 000055 126G 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 003720 IA
0000 I 000000 IX 0000 Y 000002 J 0000 000022 INJPS

```

00101 1* SUBROUTINE PULVER
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7), COSTA(7)
00105 4* IX=11
00106 5* 1000 FORMAT(/ 25H PULVERIZER ,F10.3,15H POUNDS/HOUR ,10H
00107 6* 1 SS ,6F10.3)
00110 7* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00111 8* COST(1)=COST(1)*.001
00112 9* COST(2)= COST(1)*AA(IX,11)
00113 10* COST(3)= COST(1)*AA(IX,12)
00114 11* COST(4)= COST(1)*AA(IX,13)
00115 12* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00116 13* COST(6)= COST(5)*AA(IX,15)
00121 14* DO 1 I=1,6
00123 15* 1 COSTA(I)=COST(I)+COSTA(I)
00132 16* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00133 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S SCREW,SCREW
FOR S9A-07/12-11:04 (0,)

SUBROUTINE SCREW ENTRY POINT 000246

STORAGE USED: CODE(1) 000257; DATA(0) 000126; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NIO1\$
0010 NIO2\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	00052	1000F	0000	000020	1001F	0000	000003	1002F	0000	000035	1006F	0001	000212	13L
0001	00024	14L	0001	00017	140G	0001	000135	150G	0001	000161	162G	0001	000201	174G
0001	00020	206G	0001	00006	31L	0003	R	000000	AA	0003	R	004704	BB	0004
0004	R	00007	COSTA	0000	I	000001	I	0003	I	0000	I	000105	INJPS	0000
0000	I	000002	J											

```

00101 SUBROUTINE SCREW
00103 COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 COMMON/BLOCK2/ COST(7), COSTA(7)
00105 IX=17
00106 IF(AA(IX,18).LT.6.1) GO TO 31
00110 AA(17,7) = 270.
00111 AA(17,8) = 0.80
00112 IF(AA(IX,18).LT.12.1) GO TO 31
00114 AA(17,7) = 290.
00115 AA(17,8) = 0.75
00116 IF(AA(IX,18).LT.14.1) GO TO 31
00120 AA(17,7) = 300.
00121 AA(17,8) = 0.60
00122 31 CONTINUE
00123 IF(IA(17,5).EQ.2) BB(2) = 5.0
00125 IF(IA(17,5).EQ.5) RB(2) =5.3
00127 COST(1) = BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00130 COST(1)=COST(1)*.001
00131 COST(1)=BB(2)*COST(1)
00132 COST(2) = COST(1)*AA(IX,11)
00133 COST(3) = COST(1)*AA(IX,12)
00134 COST(4) = COST(1)*AA(IX,13)

```

Table I.--Continued.

```

00135 23* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00136 24* COST(6)= COST(1)*AA(IX,15)
00137 25* DO 1 I=1,6
00142 26* 1 COSTA(I)=COST(I)+COSTA(I)
00144 27* IF(IA(17,5).EQ.5) PRINT 1006, AA(17,17),(COST(J),J=1,6)
00154 28* IF(IA(17,5).EQ.5) GO TO 14
00156 29* IF(IA(17,5).EQ.3) PRINT 1002,AA(IX,17),(COST(J),J=1,6)
00166 30* IF(IA(17,5).EQ.3) GO TO 14
00170 31* 1002 FORMAT(/25H SCREW PRESS ,F10.0,15H FEET ,10H
00170 32* C SST ,6F10.3)
00171 33* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00200 34* IF(IA(17,5).EQ.2) GO TO 13
00202 35* GO TO 14
00203 36* 13 PRINT 1001,AA(17,17),(COST(J),J=1,6)
00212 37* 1001 FORMAT(/ 25H SCREW PRESS ,F10.3,15H FEET ,10H
00212 38* 1 STEEL ,6F10.3)
00213 39* 14 CONTINUE
00214 40* IA(17,5) = 1
00215 41* 1006 FORMAT(/25H PULP PRFS ,F10.3,15H FEET ,10H
00215 42* 1 STEEL ,6F10.3)
00216 43* 1000 FORMAT(/ 25H SCREW CONVEYFR ,F10.3,15H FEET ,10H
00216 44* 1 SS ,6F10.3)
00217 45* BB(2)=1.
00220 46* RETURN
00221 47* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

@FOR,S HAMMER,HAMMER
FOR S9A-07/12-11:04 (0,)

SUBROUTINE HAMMER ENTRY POINT 000107

STORAGE USED: CODE(1) 000114; DATA(0) 000034; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 0005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000007 121G 0001 000071 130G 0001 000034 2L 0003 R 000000 AA
0003 R 004704 BB 0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 00372U IA
0000 000023 INJP\$ 0000 I 000000 IX 0000 I 000002 J

```

00101 1* SUBROUTINE HAMMER
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 18
00106 5* IF(AA(18,17).LT.1.) COST(1)=.5
00110 6* IF(AA(18,17).LT.1.) GO TO 2
00112 7* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00113 8* COST(2)=COST(1)*AA(IX,11)
00114 9* COST(3) = COST(1)*AA(IX,12)
00115 10* COST(4) = COST(1)*AA(IX,13)
00116 11* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00117 12* COST(6) = COST(5)*AA(IX,15)
00120 13* DO 1 I=1,6
00123 14* 1 COSTA(I)=COST(I)+COSTA(I)
00125 15* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00134 16* 1000 FORMAT(/25H HAMMER MILL ,F10.3,15H TONS PER HR. ,10H
00134 17* C SST ,6F10.3)
00135 18* RETURN
00136 19* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S DRYER, DRYER
FOR S9A-07/12-11:04 (0,)

SUBROUTINE DRYER ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000043 1176 0001 000055 1266 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 P 000000 AA
0000 I 000000 IX 0000 I 000002 J 0000 I 000000 I 0003 003720 IA
0000 000022 INJPS

```

00101 1* SUBROUTINE DRYER
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=19
00106 5* 1000 FORMAT(/ 25H DRUM DRYER ,F10.3,15H SQUARF FEET ,10H
00106 6* 1 SS ,6F10.3)
00107 7* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)*AA(IX,8)
00110 8* COST(1)=COST(1)*.001
00111 9* COST(2)= COST(1)*AA(IX,11)
00112 10* COST(3)= COST(1)*AA(IX,12)
00113 11* COST(4)= COST(1)*AA(IX,13)
00114 12* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00115 13* COST(6)= COST(5)*AA(IX,15)
00116 14* DO 1 I=1,6
00121 15* 1 COSTA(I)=COST(I)+COSTA(I)
00123 16* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S DRYERP,DRYERP
FOR S9A-07/12-11:04 (0,)

SUBROUTINE DRYERP ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000043 1176 0001 000055 126G 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 0000 000022 INJPS
0000 I 000000 IX 0000 I 000002 J

00101 1* SUBROUTINE DRYERP
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=20
00106 5* 1000 FORMAT(/ 25H PAN DRYFR ,F10.3,15H SQUARF FEET ,10H
00107 6* 1 SS ,6F10.3)
00110 7* COST(1)= BB(1)*AA(TX,7)*AA(IX,17)**AA(IX,8)
00111 8* COST(1)=COST(1)*.001
00112 9* COST(2)= COST(1)*AA(TX,11)
00113 10* COST(3)= COST(1)*AA(TX,12)
00114 11* COST(4)= COST(1)*AA(TX,13)
00115 12* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00116 13* COST(6)= COST(5)*AA(TX,15)
00121 14* DO 1 I=1,6
00123 15* 1 COSTA(I)=COST(I)+COSTA(I)
00132 16* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00133 17* RETURN
00133 18* END

END OF COMPILATION: NO DIAGNOSTICS.

Table 1.-- Continued.

FOR S DRYER DRYERR
FOR S9A-07/12-11:04 (0,)

SUBROUTINE DRYERR ENTRY POINT 000300

STORAGE USED: CODE(1) 000305; DATA(0) 000153; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000052 1000F 0000 000121 1001F 0000 000067 1003F 0000 000104 1004F 0001 000073 122G
0001 000247 13L 0001 000111 132G 0001 000261 14L 0001 000127 142G 0001 000145 152G
0001 000176 171G 0001 000222 203G 0001 000242 217G 0001 000255 227G 0000 000003 3006F
0000 000020 3007F 0000 000035 3008F 0004 R 000000 AA 0004 R 004704 BB 0003 R 000000 COST
0003 R 000007 COSTA 0000 I 000001 I 0004 I 003720 IA 0000 I 000142 INJF\$
0000 I 000002 J

00101 1* SUBROUTINE DRYERR
00103 2* COMMON/BLOCK2/ COST(7),COSTA(7)
00104 3* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105 4* IX=21
00106 5* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1)=COST(1)*.001
00110 7* COST(1)=BB(2)*COST(1)
00111 8* COST(2)= COST(1)*AA(IX,11)
00112 9* COST(3)= COST(1)*AA(IX,12)
00113 10* COST(4)= COST(1)*AA(IX,13)
00114 11* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00115 12* IF(IA(21,5).GE.6.AND. IA(21,5).LE.8) RB(2)=3.2*RB(2)
00117 13* COST(1)=BB(2)*COST(1)
00120 14* COST(6)= COST(5)*AA(IX,15)
00121 15* DO I I=1,6
00124 16* 1 COSTA(I)=COST(I)+COSTA(I)
00126 17* IF(IA(21,5).EQ.6) PRINT 3006,AA(21,17),(COST(I),I=1,6)
00136 18* IF(IA(21,5).EQ.7) PRINT 3007,AA(21,17),(COST(I),I=1,6)
00146 19* IF(IA(21,5).EQ.8) PRINT 3008,AA(21,17),(COST(I),I=1,6)
00156 20* IF(IA(21,5).GE.6) GO TO 14
00160 21* 3006 FORMAT(/25H DRYER
 ,F10.3,25H AREA(SQ.FEET SST

Table I.-- Continued.

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00160      C      ,6(F10.3))
00161 3007 FORMAT(/25H STRIPPER DRYER      ,F10.3,25H AREA(SQ.FEET  SST
00162      C      ,6(F10.3))
00163 3008 FORMAT(/25H CONDITIONER        ,F10.3,25H AREA(SQ.FEET  SST
00164      C      ,6(F10.3))
00165      IF(IA(21,5),F0.2) GO TO 13
00166      IF(IA(21,5),F0.3) PRINT 1003,AA(IX,17),(COST(J),J=1,6)
00167      IF(IA(21,5),F0.3) GO TO 14
00168      IF(IA(21,5),F0.4) PRINT 1004,AA(IX,17),(COST(J),J=1,6)
00169      IF(IA(21,5),F0.4) GO TO 14
00170 1000 FORMAT(/ 25H ROTARY VACUUM DRYER  ,F10.3,15H SQUARE FEET  ,10H
00171      C SS      ,6F10.3)
00172 1003 FORMAT(/ 25H STEAM TUBE DRYER    F10.3,15H SQUARE FEET  ,10H
00173      C STEEL ,6F10.3)
00174 1004 FORMAT(/25H STEAM COOKER        ,F10.0,15H SQUARE FEET  ,10H
00175      C SST  ,6F10.3)
00176      PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00177      GO TO 14
00178 13 PRINT 1001,AA(21,17),(COST(J),J=1,6)
00179 1001 FORMAT(/ 25H STEAM COOKER
00180      C STEEL ,6F10.3)
00181 14 CONTINUE
00182      IA(21,5)= 1
00183      BB(2)=1.
00184      BB(3)=1.
00185      RETURN
00186      END
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```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

BOILER, S BOILER, BOILER
FOR S9A-07/12-11:04 (0.)

SUBROUTINE BOILER ENTRY POINT 000114

STORAGE USED: CODE(1) 000120; DATA(0) 000040; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00004 1000F 0001 000060 1226 0001 000077 1326 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000002 I 0003 003720 IA 0000 000030 INUP\$
0000 I 000000 IX 0000 I 000003 J 0000 R 000001 S

00101 1* SUBROUTINE BOILER
00103 2* COMMON/BLOCK1/ AA(10,20),IA(10,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=27
00106 5* S=AA(27,7) +(0.3*AA(27,18))
00107 6* IF(AA(27,18).GT.150.) S= 500.
00111 7* IF(AA(27,18).GT.300.) S= 560.
00113 8* S=0.001*S
00114 9* COST(1)= S*BB(1)*AA(27,17)*AA(27,8)
00115 10* COST(2)= COST(1)*AA(27,11)
00116 11* COST(3)= COST(1)*AA(27,12)
00117 12* COST(4)= COST(1)*AA(27,13)
00120 13* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00121 14* DO 1 I=1,6
00124 15* COST(6)= COST(5)*AA(27,15)
00125 16* 1 COSTA(I) =COSTA(I) + COST(I)
00127 17* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00136 18* 1000 FORMAT(/25H BOILER ,F10.3,15H POUNDS/HOUR ,10H
00137 19* 1 SS ,6F10.3)
00138 20* RETURN
00140 21* END

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S EVPSR*EVPSR
FOR 59A-07/12-11:04 (0,)

SUBROUTINE EVPSR ENTRY POINT 000070

STORAGE (USED: CODE(1) 000075; DATA(0) 000031; BLANK COMMON(2) 000000)

COMMON BLOCKS:

0003 RLOCK2 000016
0004 RLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00003 1000F 0001 000040 115G 0001 000052 124G 0004 R 000000 AA 0004 R 004704 RB
0003 R 000000 COST 0003 R 000007 COSTA 0000 I 000001 Y 0004 R 003720 IA 0000 000021 INJPS
0000 I 000000 IX 0000 I 000002 J

```

00101 SUBROUTINE FVPSR
00103 COMMON /BLOCK2/ COST(7),COSTA(7)
00104 COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00105 IX=30
00106 COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 COST(2) = COST(1)*AA(IX,11)
00110 COST(3) = COST(1)*AA(IX,12)
00111 COST(4) = COST(1)*AA(IX,13)
00112 COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113 COST(6) = COST(5)*AA(IX,15)
00114 DO 1 I=1,6
00117 1 COSTA(I)=COST(I)+COSTA(I)
00121 PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00130 FORMAT(/25H SPRAY EVAPORATOR ,F10.2,15H LB/HR EVAP. ,10H
00131 CSST ,6F10.3)
00132 RETURN
00133 END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR, S EVPFLM, EVPFLM
FOR 59A-07/12-11:05 (0,)

SUBROUTINE EVPFLM ENTRY POINT 000067

STORAGE USED: CODE(1) 000073; DATA(0) 000030; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00003 1000F 0001 000044 1176 0001 000052 124G 0004 R 004704 RB
0003 R 000000 COST 0003 R 000007 COSTA 0000 I 000002 I 0004 R 000000 AA 0000 003720 IA
0000 I 000000 IX 0000 I 000001 J 0004 R 000000 IA 0000 000021 INJPS

```

00101 1* SUBROUTINE EVPFLM
00103 2* COMMON /BLOCK2/ COST(7), COSTA(7)
00104 3* COMMON /BLOCK1/ AA(100,20), IA(100,5), RB(100)
00105 4* IX=31
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(2) = COST(1)*AA(IX,11)
00110 7* COST(3) = COST(1)*AA(IX,12)
00111 8* COST(4) = COST(1)*AA(IX,13)
00112 9* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113 10* COST(6) = COST(5)*AA(IX,15)
00114 11* PRINT 1000, AA(IX,17), (COST(J), J=1,6)
00123 12* DO 1 I=1,6
00126 13* 1 COSTA(I)=COST(I)+COSTA(I)
00130 14* 1000 FORMAT(/25H WIPE FILM EVAPORATOR ,F10.2,15H SQUARE FT. ,10H
00130 15* ,6F10.3)
00131 16* CSST
00132 17* RETURN
END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S EVPFRC,EVPFRC
FOR S9A-07/12-11:05 (0,)

SUBROUTINE EVPFRC ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000042 116G 0001 000054 125G 0003 R 000000 AA 0003 R 004704 RB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 R 003720 IA 0000 000021 INJPS\$
0000 I 000000 IX 0000 I 000002 J

```

00101 1* SUBROUTINE EVPFRC
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 32
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H FORCEN CTR. FVAPORATOR ,F10.3,15H SURFACE SQ FT.,10H
00131 16* ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR, S EVPHOR, EVPHOR
FOR S9A-07/12-11:35 (0,)

SUBROUTINE EVPHOR ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00003 1000F 0001 000042 116G 0001 000054 125G 0003 R 000000 AA 0003 R 004704 RB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 003720 IA 0000 000021 INJPS
0000 I 000000 IX 0000 Y 000002 J

```

00101 1* SUBROUTINE EVPHOR
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 33
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(25H VERTICAL EVAPORATOR ,F10.3,15H SURFACE SQ FT.,10H
00131 16* C SST 6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S STORAGE STORAGE
FOR S9A-07/12-11:05 (0,)

SUBROUTINE STORAGE ENTRY POINT 000177

STORAGE USED: CODE(1) 000204; DATA(0) 000104; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001 000012 10L 0001 000121 1001I 0000 000004 1010F 0000 000021 1011F 0000 000036 1028F
0000 000053 1029F 0001 000064 130G 0001 000114 147G 0001 000130 157G 0001 000144 167G
0001 000160 177G 0001 000016 20L 0001 000041 21L 0001 000151 28L 0001 000135 29L
0001 000165 30L 0003 R 000000 AA 0003 R 004704 BB 0000 R 000001 CAST 0004 R 000000 COST
0004 R 000007 COSTA 0000 I 000002 I 0003 I 003720 IA 0000 I 000074 INJP\$
0000 I 000003 J

00101 1* SUBROUTINE STORAGE
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* AA(40,17) = AA(40,17)*0.01
00106 5* IF (AA(40,17) .GT. 10.0) GO TO 10
00110 6* IX = 40
00111 7* GO TO 20
00112 8* IX = 41
00113 9* AA(41,17) = AA(40,17)
00114 10* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00115 11* CAST = COST(1)
00116 12* C SST MATERIAL FACTOR = AA(40,18); INDEX = IA(40,U) = 1
00117 13* IF (IA(40,1) - 1) 21,22,21
00118 14* COST(1) = COST(1)*AA(IX,18)
00119 15* COST(2) = COST(1)*AA(IX,11)
00120 16* COST(3) = CAST*AA(IX,12)
00121 17* COST(4) = COST(1)*AA(IX,13)
00122 18* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00123 19* COST(6) = COST(5)*AA(IX,15)
00124 20* DO 1 I=1,6
00125 21* COSTA(I)=COST(I)+COSTA(I)
00126
00127
00132

Table I.--Continued.

```

00134 22* AA(IX,17) = AA(IX,17)*100.0
00135 23* IF(IA(40,2) .EQ. 1) GO TO 29
00137 24* IF(IA(40,2) .EQ. 2) GO TO 28
00141 25* IF (IA(40,1) - 1)1000,1001,1000
00144 26* PRINT 1010,AA(IX,17),(COST(J),J=1,6)
00153 27* GO TO 30
00154 28* PRINT 1011,AA(IX,17),(COST(J),J=1,6)
00163 29* GO TO 30
00164 30* PRINT 1029,AA(IX,17),(COST(J),J=1,6)
00173 31* GO TO 30
00174 32* PRINT 1028,AA(IX,17),(COST(J),J=1,6)
00203 33* GO TO 30
00204 34* FORMAT(/25H SHOP FAR. STORAGE TANK ,F10.0,15H GALLONS ,10H
00205 35* C STEEL ,6F10.3)
00206 36* FORMAT(/25H SHOP FAR. STORAGE TANK ,F10.0,15H GALLONS ,10H
00207 37* C SST ,6F10.3)
00208 38* FORMAT(/25H WATER DUMP TANK ,F10.0,15H GALLONS ,10H
00209 39* CSTEEL ,6F10.3)
00210 40* FORMAT(/25H ACID STORAGE TANK ,F10.0,15H GALLONS ,10H
00211 41* C SST ,6F10.3)
00212 42* CONTINUE
00213 43* RETURN
00214 44* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S VESSEL, VESSEL
FOR 59A-07/12-11:05 (0.)

SUBROUTINE VESSEL ENTRY POINT 000210

STORAGE USED: CODE(1) 000215; DATA(0) 000065; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000004	1000F	0001	000141	144G	0001	000157	156G	0001	000172	165G	0000	000021	2000F
0001	000077	3L	0001	000105	4L	0001	000163	5L	0003	R	000000	AA	0003	R 004704 BB
0004	R	000000	COST	0004	P	000007	COSTA	0000	R	000001	F	0000	I	003720 IA
0000	000054	INJP\$	0000	I	000000	IX	0000	R	000002	I				

00101	1*	SUBROUTINE VESSEL
00103	2*	COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104	3*	COMMON/BLOCK2/ COST(7),COSTA(7)
00105	4*	IX=42
00106	5*	IF(IA(42,3).EQ.1) F=AA(42,1)
00110	6*	IF(IA(42,3).EQ.2) F=AA(42,2)
00112	7*	IF(IA(42,3).EQ.3) F=AA(42,3)
00114	8*	UF=AA(42,18)**1.6*AA(42,19)*0.132
00115	9*	IF(IA(42,2).EQ.1) COST(1)=.313*U**0.81 *BB(1)
00117	10*	IF(IA(42,2).EQ.2) COST(2)=.260*U**0.759*BB(1)
00121	11*	IF(IA(42,2).NF.1) GO TO 3
00123	12*	AA(42,11)= 1.038
00124	13*	AA(42,12)= .992
00126	14*	AA(42,13)= 1.20
00127	15*	GO TO 4
00130	16*	3 AA(42,11) = 0.645
00131	17*	AA(42,12) = 0.615
00132	18*	AA(42,13) = 0.916
00133	19*	4 CONTINUE
00134	20*	COST(4)= COST(1)* AA(IX,13)
00135	21*	COST(3)= COST(1)* AA(IX,12)
00136	22*	COST(2)= COST(1)* AA(IX,11)
00136	23*	COST(1) =COST(1)*F

Table I.--Continued.

```

00137      COST(5)=COST(1)+COST(2)+COST(3)+COST(4)
00140      AA(42,17)=3.14159*.25*AA(42,18)*AA(42,18)*AA(42,19)
00141      COST(7)=0.
00142      COST(6)= COST(1)*AA(1X,15)
00143      DO 1 I=1,7
00146      1 COSTA(I) = COSTA(I) +COST(I)
00150      1000 FORMAT(/ 25H PRESSURE VESSEL      ,F10.3,15H CUBIC FEET  ,10H
00151      1 SS      ,6F10.3)
00152      IF(IA(42,4).EQ.2) GO TO 5
00153      PRINT 1000, AA(1X,17), (COST(I),I=1,6)
00162      5 PRINT 2000, AA(1X,17),(COST(I),I=1,6)
00171      2000 FORMAT(/25H DIST. COLUMN SHELL  ,F10.3,15H CUBIC FEET  ,10H
00171      1 SS      ,6F10.3)
00172      RETURN
00173      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S COLUMN COLUMN
FOR S9A-07/12-11:05 (0,)

SUBROUTINE COLUMN ENTRY POINT 000157

STORAGE USED: CODE(1) 000163; DATA(0) 000044; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000005 1000F 0001 000130 1366 0001 000142 1456 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 R 000002 FM 0000 R 000001 FS
0000 I 000004 I 0003 I 003720 IA 0000 000034 INJP\$ 0000 I 000000 IX

00101 1* SUBROUTINE COLUMN ,10H
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=43
00106 5* 1000 FORMAT(/ 25H DISTILLATION COLUMN ,F10.3,15H FEET(HIGHT) ,10H
00106 6* 1 SS ,6F10.3)
00107 7* FS=1.0+ (0.4)**((24.-AA(43,18))/6.)
00110 8* FM=AA(43,1)
00111 9* FT=0.
00112 10* IF(AA(43,2).GT.2.) FT=AA(43,4)
00114 11* IF(AA(43,2).GT.4.) FT=AA(43,5)
00116 12* IF(IA(43,3).EQ.2) FM=0.
00120 13* IF(AA(43,17).LE.4.) AA(43,7)=8.3*(AA(43,20))
00122 14* IF(AA(43,17).GE.4.) AA(43,7)=AA(43,20)*(AA(43,20)+4.3)
00124 15* COST(1)= (AA(43,17))*AA(43,8)+AA(43,7)*BB(1)*(FS+FT)
00125 16* COST(1)=COST(1)*.001
00126 17* COST(2)= COST(1)* AA(IX,11)
00127 18* COST(3)= COST(1)* AA(IX,12)
00130 19* COST(4)= COST(1)* AA(IX,13)
00131 20* COST(7)=0.
00132 21* COST(1)= COST(1)*1.+FM
00133 22* COST(5)=COST(1)+COST(2)+COST(3)+COST(4)
00134 23* COST(6)= COST(1)*AA(IX,15)
00135 24* DO 1 I=1,7

Table I.-- Continued.

```
00140      25*      1  COSTA(I) = COSTA(I) +COST(I)
00142      26*      PRINT 1000, AA(43,17),(COST(I),I=i,6)
00151      27*      RETURN
00152      28*      END
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S REACTR,REACTR
FOR S9A-07/12-11:05 (0,)

SUBROUTINE REACTR ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000042 116G 0001 000054 125G 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 R 000000 AA
0000 I 000000 IX 0000 T 000002 J 0000 I 000001 I 0000 000021 INJPS

```

00101 1* SUBROUTINE REACTR
00103 2* COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=49
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(49,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 100,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H JACKETED REACTOR VESSEL ,F10.0,15H GALLONS ,10H
00131 16* CSST ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S GRINDR/GRINDR
FOR S9A-07/12-11:05 (0,)

SUBROUTINE GRINDR ENTRY POINT 000070

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000042 116G 0001 000054 125G 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 003720 IA 0000 000021 INJPS
0000 I 000000 IX 0000 I 000002 J

```

00101 SUBROUTINE GRINDR
00103 COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 COMMON /BLOCK2/ COST(7),COSTA(7)
00105 IX=50
00106 COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 COST(1) = COST(1)*AA(50,18)
00110 COST(2) = COST(1)*AA(IX,11)
00111 COST(3) = COST(1)*AA(IX,12)
00112 COST(4) = COST(1)*AA(IX,13)
00113 COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 COST(6) = COST(5)*AA(IX,15)
00115 DO 1 I=1,6
00120 1 COST(I)=COST(I)+COSTA(I)
00122 PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 1000 FORMAT(/25H FISH GRINDER ,F10.3,15H TONS/HR ,10H
00131 ,6F10.3)
00132 RETURN
00133 END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S SCREEN/SCREEN
FOR S9A-07/12-11:05 (0,)

SUBROUTINE SCREEN ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 MEXP6\$
0006 NPRT\$
0007 NIO1\$
0010 NIO2\$
0011 MERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000042 116G 0001 000054 125G 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 003720 IA 0000 000021 INJPS
0000 I 000000 IX 0000 I 000002 J

00101 1* SUBROUTINE SCREEN
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 51
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)*AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H VIBRATING SCREEN ,F10.3,15H SURFACE SQ FT.,10H
00131 16* C SST ,6F10.3)
00132 17* RETURN
00133 18* END

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S SHARP, SHARP
FOR S9A-07/12-11:05 (0,)

SUBROUTINE SHARP ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NIO1\$
0010 NIO2\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00003 1000F 0001 000043 116G 0001 000055 125G 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0000 003720 IA 0000 000022 INJPS
0000 I 000000 IX 0000 I 000002 J

```

00101 1* SUBROUTINE SHARP
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=52
00106 5* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1)=COST(1)*.001
00110 7* COST(2)= COST(1)*AA(IX,11)
00111 8* COST(3)= COST(1)*AA(IX,12)
00112 9* COST(4)= COST(1)*AA(IX,13)
00113 10* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00114 11* COST(6)= COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H SHARPLES CENTRIFUGE ,F10.3,15H HORSEPOWER ,10H
00131 16* 1 SS ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DRAENOSTTCS.

Table I.--Continued.

FOR,S ROWL,BOWL
FOR S9A-07/12-11:05 (0,)

SUBROUTINE BOWL ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK1 005050
0004 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 MEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000043 116G 0001 000055 125G 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 R 000000 AA
0000 I 000000 IX 0000 I 000002 J 0000 I 000001 I 0003 000022 INJPS

```

00101 1* SUBROUTINE BOWL
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=53
00106 5* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1)=COST(1)*.001
00110 7* COST(2)= COST(1)*AA(IX,11)
00111 8* COST(3)= COST(1)*AA(IX,12)
00112 9* COST(4)= COST(1)*AA(IX,13)
00113 10* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00114 11* COST(6)= COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H SOLID BOWL CENTRIFUGE ,F10.3,15H HORSEPOWER ,10H
00131 16* 1 SS ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S CNTFGE,CNTFGE
FOR S9A-07/12-11:05 (0,)

SUBROUTINE CNTFGE ENTRY POINT 000067

STORAGE USED: CODE(1) 000074; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NIO1\$
0010 NIO2\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000017 116G 0001 000051 125G 0003 R 000000 AA 0003 R 004704 RB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 003720 IA 0000 000022 INJPS
0000 I 000000 IX 0000 I 000002 J

00101 SUBROUTINE CNTFGE
00103 COMMON/BLOCK1/ AA(10,20),IA(10,5),BB(100)
00104 COMMON/BLOCK2/ COST(7), COSTA(7)
00105 IX=54
00106 COST(1)= BB(1)*AA(54,7)*AA(54,17)**AA(54,8)
00107 COST(1)=COST(1)**.001
00110 COST(2)= COST(1)* AA(54,11)
00111 COST(3)= COST(1)* AA(54,12)
00112 COST(4)= COST(1)* AA(54,13)
00113 COST(5)= COST(1) + COST(2) + COST(3)+COST(4)
00114 COST(6)= COST(5)* AA(54,15)
00115 DO 1 I=1,6
00120 1 COSTA(I)=COST(I) + COSTA(I)
00122 PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131 1000 FORMAT(/25H DISK TYPE CENTRIFUGE ,F10.3,15H HORSEPOWER ,10H
00131 1 SS ,6F10.3)
00132 RETURN
00133 END

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

3FOR,S BLENDR,BLENDR
FOR S9A-07/12-11:05 (0,)

SUBROUTINE BLENDR ENTRY POINT 000070

STORAGE USED: CODE(1) 000075; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 00003,1000F 0001 000000 115G 0001 000052 124G 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 R 003720 IA 0000 I 000021 INJPF
0000 I 000000 IX 0000 I 000002 J 0000 I 000001 I

00101 1* SUBROUTINE BLENDR
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 57
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(2) = COST(1)*AA(IX,11)
00110 7* COST(3) = COST(1)*AA(IX,12)
00111 8* COST(4) = COST(1)*AA(IX,13)
00112 9* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113 10* COST(6) = COST(5)*AA(IX,15)
00114 11* DO 1 I=1,6
00117 12* 1 COSTA(I)=COST(I)+COSTA(I)
00121 13* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00130 14* 1000 FORMAT(/25H SOLIDS BLENDR ,F10.3,15H CUBIC FT / HR.,10H
00131 15* C SST ,6F10.3)
00131 16* RETURN
00132 17* END

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S PMPRFC,PMPREC
FOR S9A-07/12-11:05 (0,)

SUBROUTINE PMPREC ENTRY POINT 000212

STORAGE USED: CODE(1) 000217; DATA(0) 000107; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 ALOG
0006 NEXP6\$
0007 NPRT\$
0010 NI01\$
0011 NI02\$
0012 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000005	1000F	0000	000022	1001F	0000	000037	1002F	0000	000054	1003F	0001	000054	11L
0001	000060	12L	000J	000103	130G	0001	000135	14L	0001	000130	145G	0001	000151	15L
0001	000144	155G	0001	000200	16L	0001	000160	165G	0001	000165	17L	0001	000174	175G
0003	R	000000	AA	0003	R	004704	RB	0000	R	000000	COST	0004	R	000007
0000	R	000000	EXP	0000	T	000003	I	0003	I	000720	IA	0000	I	000001
0000	I	000004	J									0000	I	000001

00101	1*	SUBROUTINE PMPREC
00103	2*	COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104	3*	COMMON /BLOCK2/ COST(7),COSTA(7)
00105	4*	IX = 65
00106	5*	AA(IX,17) = AA(IX,17)*0.001
00107	6*	EXP = AA(IX,8) + AA(IX,9)*LOG(AA(IX,17))
00110	7*	COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**EXP
00111	8*	IF(AA(IX,17) .LT. 0.1) COST(1) = 0.9
00113	9*	COST = COST(1)
00114	10*	IF (IA(IX,1) = 1) 12,11,10
00117	11*	COST(1) = COST(1)*AA(IX,19)
00120	12*	GO TO 12
00121	13*	COST(1) = COST(1)*AA(IX,18)
00122	14*	COST(2) = COST(1)*AA(IX,11)
00123	15*	COST(3) = COST*AA(IX,12)
00124	16*	COST(4) = COST(1)*AA(IX,13)
00125	17*	COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00126	18*	COST(6) = COST(5)*AA(IX,15)
00127	19*	DO 1 I=1,6
00132	20*	1 COSTA(I)=COST(I)+COSTA(I)

Table I.--Continued.

```

00134      21*      AA(IX,17) = 1000.0*AA(IX,17)
00135      22*      IF (IA(IX,2) .EQ. 1) GO TO 17
00137      23*      IF (IA(IX,1) - 1) 13,14,15
00142      24*      13      PRINT 1000*AA(IX,17), (CONST(J), J=1,6)
00151      25*      GO TO 16
00152      26*      14      PRINT 1001*AA(IX,17), (CONST(J), J=1,6)
00161      27*      GO TO 16
00162      28*      15      PRINT 1002*AA(IX,17), (CONST(J), J=1,6)
00171      29*      GO TO 16
00172      30*      17      PRINT 1003*AA(IX,17), (CONST(J), J=1,6)
00201      31*      16      CONTINUE
00202      32*      1000  FORMAT(/25H RECIPROCATING PUMP
00203      33*      C STEEL
00203      34*      ,6F10.3)
00203      35*      1001  C BRONZE
00204      36*      ,6F10.3)
00204      37*      1002  C SST
00205      38*      ,6F10.3)
00205      39*      1003  C STEEL
00206      40*      ,6F10.3)
00207      41*      RETURN
          END
          ,F10.0,15H GPM TIMES PSI ,10H
          ,F10.0,15H GPM TIMES PSI ,10H
          ,F10.0,15H GPM TIMES PSI ,10H
          ,F10.0,15H GPM TIMES PSI ,10H

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S PMPCNT,PMPCNT
FOR S9A-07/12-11:05 (0,)

SUBROUTINE PMPCNT ENTRY POINT 000012

STORAGE USED: CODE(1) 000217; DATA(0) 000107; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 AL0G
0006 NEXP6\$
0007 MPRT\$
0010 NI01\$
0011 NI02\$
0012 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000022	1000F	0000	000007	1001F	0000	000054	1002F	0000	000005	1003F	0001	000054	11L
0001	000060	12L	0001	000103	130G	0001	000151	14L	0001	000130	145G	0001	000165	15L
0001	000144	155G	0001	000200	16L	0001	000160	166G	0001	000135	17L	0001	000174	176G
0003	R	000000	AA	0003	R	004704	BR	0000	R	000002	CAST	0004	R	000007
0000	R	000000	EXP	0000	I	000003	I	0003	I	000720	TA	0000	I	000001
0000	I	000004	J									0000	I	000001

00101	1*	SUBROUTINE PMPCNT
00103	2*	COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104	3*	COMMON /BLOCK2/ COST(7),COSTA(7)
00105	4*	IX = 66
00106	5*	AA(IX,17) = AA(IX,17)*0.001
00107	6*	EXP = AA(IX,8) + AA(IX,9)*LOG(AA(IX,17))
00110	7*	COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**EXP
00111	8*	IF(AA(IX,17) .LT. 0.1) COST(1) = 0.4
00113	9*	CAST = COST(1)
00114	10*	IF (IA(IX,1) - 1) 12,11,10
00117	11*	COST(1) = COST(1)*AA(IX,19)
00120	12*	GO TO 12
00121	13*	COST(1) = COST(1)*AA(IX,1A)
00122	14*	COST(2) = COST(1)*AA(IX,11)
00123	15*	COST(3) = CAST*AA(IV,12)
00124	16*	COST(4) = COST(1)*AA(IX,13)
00125	17*	COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00126	18*	COST(6) = COST(5)*AA(IX,15)
00127	19*	DO 1 I=1,6
00132	20*	1 COSTA(I)=COST(I)+COSTA(I)

Table I.--Continued.

```

00134      AA(IX,17) = 1000.0*AA(IX,17)
00135      IF(IA(66,4),F0.2) GO TO 17
00137      IF(IA(IX,1) - 1) 13,14,15
00142      PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00151      GO TO 16
00152      17 PRINT 1003,AA(IX,17),(COST(J),J=1,6)
00161      GO TO 16
00162      1003 FORMAT(/25H SFA WATER PUMPS      ,F10.3,15H GPM TIMES PSI ,10H
00163      1 BRONZE      ,6F10.3)
00172      14 PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00173      GO TO 16
00202      15 PRINT 1002,AA(IX,17),(COST(J),J=1,6)
00203      16 CONTINUE
00203      1000 FORMAT(/25H CFNTRIFUGAL PUMP      ,F10.3,15H GPM TIMES PSI ,10H
00204      C STEEL      ,6F10.3)
00204      1001 FORMAT(/25H CENTRIFUGAL PUMP      ,F10.0,15H GPM TIMES PSI ,10H
00205      C BRONZE      ,6F10.3)
00205      1002 FORMAT(/25H CENTRIFUGAL PUMP      ,F10.3,15H GPM TIMES PSI ,10H
00206      C SST      ,6F10.3)
00207      RETURN
      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S HEATEX,HEATEX
FOR S9A-07/12-11:35 (0,)

SUBROUTINE HEATEX ENTRY POINT 000164

STORAGE USED: CODE(1) 000171; DATA(0) 000101; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000107	1001L	0001	000123	1002	0000	000004	1010F	0000	000021	1011F	0000	000036	1013F
0000	000053	1014F	0001	000025	11L	0001	000031	12L	0001	000060	126G	0001	000035	13L
0001	000102	142G	0001	000116	152G	0001	000132	162G	0001	000145	174G	0001	000152	30L
0001	000136	4L	0004	R	000000	AA	0004	R	0000	R	000001	CAST	0000	R
0003	R	000007	COSTA	0000	I	000002	I	0004	I	000720	IA	0000	I	000000
0000	I	000003	J									0000	I	000000

00101	1*	SUBROUTINE HEATEX
00103	2*	COMMON /BLOCK2/ COST(7),COSTA(7)
00104	3*	COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00105	4*	IX=67
00106	5*	COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107	6*	CAST = COST(1)
00110	7*	IF (IA(67,1) - 1) 10,11,12
00113	8*	10
00114	9*	11
00115	10*	COST(1) = COST(1)*AA(67,18)
00116	11*	60 TO 13
00117	12*	COST(1) = COST(1)*AA(67,19)
00120	13*	60 TO 13
00121	14*	COST(2) = COST(1)*AA(IX,11)
00122	15*	COST(3) = CAST*AA(IX,12)
00123	16*	COST(4) = COST(1)*AA(IX,13)
00124	17*	COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00125	18*	COST(6) = COST(5)*AA(IX,15)
00130	19*	DO 1 I=1,6
00130	19*	1 COSTA(I)=COST(I)+COSTA(I)
00130	20*	C MATERIAL FACTORS IA(67,1) = 0,1,2 IMPLIES SHELL/TURE =ST/ST,ST/SSST
00130	21*	C AND SST/SSST

Table I.--Continued.

```

00132      22*      IF (IA(67,4),F0.4) GO TO 4
00134      23*      IF (IA(67,1) - 1) 1000,1001,1002
00137      24*      1000 PRINT 1010,AA(IX,17),(COST(J),J=1,6)
00146      25*      GO TO 30
00147      26*      1001 PRINT 1011,AA(IX,17),(COST(J),J=1,6)
00156      27*      GO TO 30
00157      28*      1002 PRINT 1013,AA(IX,17),(COST(J),J=1,6)
00166      29*      1010 FORMAT(/25H HEAT EXCHANGER
00167      30*      C ST/ST
00167      31*      ,6F10.3)
00167      32*      1011 FORMAT(/25H HEAT EXCHANGER
00170      33*      C ST/SST
00170      34*      ,6F10.3)
00171      35*      1013 FORMAT(/25H HEAT EXCHANGER
00200      36*      C SST/SST
00201      37*      ,6F10.3)
00201      38*      4 PRINT 1014,AA(IX,17),(COST(J),J=1,6)
00202      39*      GO TO 30
00203      40*      1014 FORMAT(/25H VENT CONDENSER
00204      41*      1 ST/SST
                                ,6F10.3)
                                30 CONTINUE
                                RETURN
                                END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S BELT,BELT
FOR 59A-07/12-11:05 (1,)

SUBROUTINE BELT ENTRY POINT 000123

STORAGE USED: CODE(1) 000130; DATA(0) 000041; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT5
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000004 1000F 0001 000071 124G 0001 000103 133G 0003 R 004704 RB
0004 R 000000 COST 0004 P 000007 COSTA 0000 I 000002 I 0003 R 003720 IA
0000 I 000000 IX 0000 Y 000003 J 0000 R 000001 Q 0000 000027 INJPS

```

00101 1* SUBROUTINE BELT
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=70
00106 5* Q= AA(IX,7)
00107 6* IF(AA(IX,18).GT.35.) AA(IX,7)=AA(IX,7)+ 80.
00111 7* IF(AA(IX,18).GT.47.) AA(IX,7)=AA(IX,7)+ 210.
00113 8* 1000 FORMAT(/25H BELT CONVEYER ,F10.3,15H FEET(LENGTH) ,10H
00113 9* ,6F10.3)
00114 10* COST(1)= RB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00115 11* COST(1)=COST(1)*.901
00116 12* COST(2)= COST(1)*AA(IX,11)
00117 13* COST(3)= COST(1)*AA(IX,12)
00120 14* COST(4)= COST(1)*AA(IX,13)
00121 15* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00122 16* COST(6)= COST(5) * AA(IX,15)
00123 17* DO 1 I = 1,6
00126 18* 1 COSTA(I) = COST(I) + COSTA(I)
00130 19* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00137 20* AA(IX,7)=Q
00140 21* RETURN
00141 22* END

```

FND OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

DEFOR,S BUCKET,BUCKET
FOR S9A-07/12-11:05 (0,)

SUBROUTINE BUCKET ENTRY POINT 000134

STORAGE USED: CODE(1) 000141; DATA(0) 000041; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK1 005050
0004 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 R 000004 1000F 0001 000102 1246 0001 000114 1336 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000002 I 0000 I 000000 IX 0000 I 000003 J 0000 R 000001 0 0000 I 000027 INJPS

00101 1* SUBROUTINE BUCKET
00103 2* COMMON/BLOCK1/ AA(100,20),TA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=71
00106 5* 0= AA(IX,7)
00107 6* 1000 FORMAT(/25H BUCKET CONVEYFR ,F10.3,15H FFET(HEIGHT) ,10H
00107 7* 1 SS ,6F10.3)
00110 8* IF(AA(IX,18).GT.30..AND.AA(IX,18).LE.75.) AA(IX,7)=AA(IX,7)+180.
00112 9* IF(AA(IX,18).GT.75.) AA(IX,7)=AA(IX,7)+ 280.
00114 10* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)*AA(IX,8)
00115 11* COST(1)=COST(1)*.001
00116 12* COST(2)= COST(1)*AA(IX,11)
00117 13* COST(3)= COST(1)*AA(IX,12)
00120 14* COST(4)= COST(1)*AA(IX,13)
00121 15* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00122 16* COST(6)= COST(5)*AA(IX,15)
00123 17* DO 1 I=1,6
00126 18* 1 COSTA(I)=COST(I)+COSTA(I)
00130 19* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00137 20* AA(IX,7)=0
00140 21* RETURN
00141 22* END

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S SCALF,SCALE
FOR S9A-07/12-11:05 (0,)

SUBROUTINE SCALE ENTRY POINT 000116

STORAGE USED: CODE(1) 000123; DATA(0) 000036; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NPRT\$
0006 NI01\$
0007 NI02\$
0010 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000005 1000F 0001 000066 1266 0001 000100 1356 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000003 I 0003 R 000000 AA
0000 I 000002 IS 0000 I 000000 IX 0000 I 000004 J 0000 I 000001 SIZE
0000 000025 TNJPS

```

00101 1* SUBROUTINE SCALE
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=72
00106 5* 1000 FORMAT(/ 25H SCALE
00106 6* 1 SS ,6F10.3)
00107 7* SIZE=AA(IX,17)
00110 8* IS = SIZE/17.9
00111 9* IF(IS.EQ.1) COST(1)=AA(72,20)*RB(1)
00113 10* IF(IS.EQ.2) COST(1)=AA(72,18)*BB(1)
00115 11* IF(IS.EQ.3) COST(1)=AA(72,19)*BB(1)
00117 12* COST(2)= AA(72,11) * COST(1)
00120 13* COST(3)= 0.00
00121 14* COST(4)= AA(IX,13)*COST(1)
00122 15* COST(5)= COST(1)+COST(2)+COST(3) +COST(4)
00123 16* COST(6)=COST(1)*AA(IX,15)
00124 17* COST(7)=0.
00125 18* DO 1 I=1,7
00130 19* COSTA(I)=COST(I)+COSTA(I)
00132 20* PRINT 1000 , AA(IX,17),(COST(J),J=1,6)
00141 21* RETURN
00142 22* END
    ,F10.3,15H TONS
    ,10H

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S AGITOR,AGITOR
FOR S9A-07/12-11:05 (0,)

SUBROUTINE AGITOR ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK1 005050
0004 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000043 116G 0001 000055 125G 0003 R 000000 AA 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0000 003720 IA 0000 000022 INJPS
0000 I 000000 IX 0000 Y 000002 J

```

00101 1* SUBROUTINE AGITOR
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=73
00106 5* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1)=COST(1)*.01
00110 7* COST(2)= COST(1)*AA(IX,11)
00111 8* COST(3)= COST(1)*AA(IX,12)
00112 9* COST(4)= COST(1)*AA(IX,13)
00113 10* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00114 11* COST(6)= COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000, AA(IX,17), (COST(J),J=1,6)
00131 15* 1000 FORMAT(/ 25H AGITATOR-PROPELLAR ,F10.3,15H HORSEPOWER ,10H
00132 16* 1 SS ,6F10.3)
00133 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DTAGNOSTICS.

Table I.--Continued.

FOR, S BALMTL, BALMIL
FOR S9A-07/12-11:06 (0,)

SUBROUTINE BALMIL ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000002 1166 0001 000054 1256 0003 R 004704 BB
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 R 000000 AA
0000 I 000000 IX 0000 I 000002 J 0000 I 000001 I 0003 003720 IA
0000 000021 INJPS

```

00101 1* SUBROUTINE BALMIL
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 74
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)*AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* I COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 100,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 C SST ,FORMAT(/25H BALL MIL ,F10.3,15H TONS PER HR. ,10H
00131 16* ,6FIN.3)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S BAGGMA,BAGGMA
FOR S9A-07/12-11:06 (0,)

SUBROUTINE BAGGMA ENTRY POINT 000125

STORAGE USED: CODE(1) 000132; DATA(0) 000051; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 MPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0000 000020 1001F 0001 000053 120G
0003 R 009000 AA 0003 R 004704 BB 0004 R 000000 COST
0003 I 003720 IA 0000 000007 INJP\$ 0000 I 000000 IX
0001 000070 130G
0000 I 000001 I
0001 000107 140G
0000 I 000001 I

```

00101 1* SUBROUTINE BAGGMA
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=75
00106 5* IF(IA(75,2).EQ.2) AA(75,7)=AA(75,1)
00110 6* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00111 7* COST(1)=COST(1)*.001
00112 8* COST(2)= COST(1)*AA(IX,11)
00113 9* COST(3)= COST(1)*AA(IX,12)
00114 10* COST(4)= COST(1)*AA(IX,13)
00115 11* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00116 12* COST(6)= COST(5)*AA(IX,15)
00117 13* DO 1 I=1,6
00122 14* 1 COSTA(I)=COST(I)+COSTA(I)
00124 15* IF(IA(IX,1).FO.0) PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00134 16* IF(IA(IX,1).FO.1)PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00144 17* 1000 FORMAT(/ 25H BAGGING MACHINE
00144 18* ,6F10.3)
00145 19* 1001 FORMAT(/ 25H CANNING MACHINE
00145 20* CSST ,6F10.3)
00146 21* RETURN
00147 22* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S FILTER,FILTER
FOR 59A-07/12-11:06 (0,)

SUBROUTINE FILTER ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000042 1166 0001 000054 1256 0003 R 004704 8B
0004 R 000000 COST 0004 R 000007 COSTA 0000 I 000001 I 0003 R 003720 IA
0000 I 000000 IX 0000 I 000002 J 0000 0000021 INJPS

```

00101 1* SUBROUTINE FILTER
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX= 78
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H ROT. PRIM FILTER ,F10.3,15H SURFACE SQ.FT.,10H
00131 C SST ,6F10.3)
00132 16* RETURN
00133 17* END
00133 18*

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S CRANES, CRANES
FOR S9A-07/12-11:06 (0,)

SUBROUTINE CRANES ENTRY POINT 000141

STORAGE USED: CODE(1) 000146; DATA(0) 000063; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0000 000020 1001F 0000 000035 1002F 0001 000026 11L 0001 000032 12L
0001 000055 123G 0001 000073 135G 0001 000100 14L 0001 000107 145G 0001 000114 15L
0004 R 000007 COSTA 0001 000127 16L 0003 R 000000 AA 0003 R 004704 BB 0004 R 000000 COST
0000 I 000002 J 0000 I 000001 I 0003 I 000720 IA 0000 000053 INJP\$ 0000 I 000000 IX

00101 1* SUBROUTINE CRANES
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX= 80
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* IF (IA(80,1) - 1) 12,11,10
00112 7* COST(1) = COST(1)*AA(IX,19)
00113 8* GO TO 12
00114 9* COST(1) = COST(1)*AA(IX,18)
00115 10* COST(2) = COST(1)*AA(IX,11)
00116 11* COST(3) = COST(1)*AA(IX,12)
00117 12* COST(4) = COST(1)*AA(IX,13)
00120 13* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00121 14* COST(6) = COST(5)*AA(IX,15)
00122 15* DO 1 I=1,6
00125 16* COSTA(I)=COST(I)+COSTA(I)
00127 17* IF (IA(80,1) - 1) 13,14,15
00132 18* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00141 19* GO TO 16
00142 20* PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00151 21* GO TO 16
00152 22* PRINT 1002,AA(IX,17),(COST(J),J=1,6)

Table I.-- Continued.

00161	23*	16	CONTINUE						
00162	24*	1000	FORMAT(/25H OVERHEAD CRANE 20FT SPAN,F10.3,15H TONS I IFT						,10H
00162	25*	C	STEEL ,6F10.3)						
00163	26*	1001	FORMAT(/25H OVERHEAD CRANE 30FT SPAN,F10.3,15H TONS LIFT						,10H
00163	27*	C	STEEL ,6F10.3)						
00164	28*	1002	FORMAT(/25H OVERHEAD CRANE 40FT SPAN,F10.3,15H TONS LIFT						,10H
00164	29*	C	STEEL ,6F10.3)						
00165	30*		RETURN						
00166	31*		END						

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S DRAGMA DRAGMA
FOR S9A-07/12-11:06 (0.)

SUBROUTINE DRAGMA ENTRY POINT 000143

STORAGE USED: CODE(1) 000151; DATA(0) 000051; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000110 1416 0001 000122 150G
0003 R 000000 AA 0003 R 004704 BB 0004 R 000000 COST
0003 003720 IA 0000 000036 INJP\$ 0000 I 000000 IX
0001 000026 2L 0001 000050 3L
0000 I 000002 I
0000 R 000001 Q

00101 1* SUBROUTINE DRAGMA
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=81
00106 5* 0= AA(IX,7)
00107 6* IF(AA(81,18).GT.15.) GO TO 2
00111 7* AA(81,11)= 0.27
00112 8* AA(81,12)= 0.42
00113 9* IF(AA(81,1A).LE.13.) AA(81,7)=7.
00115 10* GO TO 3
00116 11* 2 CONTINUE
00117 12* IF(AA(81,18).E.20.) AA(81,7)=10.
00121 13* IF(AA(81,18).E.1A.) AA(81,7)=9.
00123 14* AA(81,11)=0.278
00124 15* AA(81,12)=0.382
00125 16* 3 CONTINUE
00126 17* 1000 FORMAT(/ 25H DRAG CONVEYER ,F10.3,15H FEET
00127 18* ,6F10.3)
00130 19* COST(1)=BB(1)*AA(81,7)*AA(81,17)**AA(81,8)
00131 20* COST(1)=COST(1)*.001
00132 21* COST(2)= COST(1)* AA(IX,11)
00133 22* COST(3)= COST(1)* AA(IX,12)
00134 23* COST(4)= COST(1)* AA(IX,13)
00134 24* COST(5)=COST(1)+COST(2)+COST(3)+COST(4)

Table I.-- Continued.

```

00135      AA(IX,15)=.1
00136      COST(7)=0.
00137      COST(6)= COST(1)*AA(IX,15)
00140      DO 1 I=1,7
00143      1 COSTA(I) = COSTA(I) +COST(I)
00145      PRINT 1000, AA(IX,17), (COST(I),I=1,6)
00154      AA(IX,7)=0
00155      RETURN
00156      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S REFRIG,REFRIG
FOR 59A-07/12-11:06 (0,)

SUBROUTINE REFRIG ENTRY POINT 000120

STORAGE USED: CODE(1) 000125; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$
0006 NPRT\$
0007 NI01\$
0010 NI02\$
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000 000003 1000F 0001 000046 11L 0001 000042 12L 0001 000045 13L
0001 000102 135G 0003 R 000000 AA 0003 R 004704 BB 0004 R 000007 COSTA
0000 I 000001 I 0003 Y 003720 IA 0000 000021 INJP\$ 0000 I 000000 IX 0000 I 000002 J

```

00101 1* SUBROUTINE REFRIG
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX =85
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* IF (IA(85,1) .GT. 40) GO TO 13
00111 7* IF (IA(85,1) .GT. 20) GO TO 11
00113 8* IF (IA(85,1) .GT. 1) GO TO 12
00115 9* COST(1) = COST(1)*AA(85,18)
00116 10* GO TO 13
00117 11* COST(1) = COST(1)*AA(85,13)
00120 12* COST(2) = COST(1)*AA(IX,11)
00121 13* COST(3) = COST(1)*AA(IX,12)
00122 14* COST(4) = COST(1)*AA(IX,13)
00123 15* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00124 16* COST(6) = COST(5)*AA(IX,15)
00125 17* DO 1 I=1,6
00130 18* COSTA(I)=COST(I)+COSTA(I)
00132 19* PRINT 1000,AA(IX,17),(COST(I),J=1,6)
00141 20* 1000 C FORMAT(/25H MECHANICAL REFRIGERAT. ,F10.3,15H TONS
00142 21* ,6F10.3)
00143 22* RETURN
00144 23* END
    
```

Table I.--Continued.

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S WATER,WATER
FOR S9A-07/12-11:06 (0,)

SUBROUTINE WATER ENTRY POINT 000113

STORAGE USED: CODE(1) 000121; DATA(0) 000151; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$
0005 NIQ2\$
0006 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000002	105G	0000	000005	1050F	0000	000020	1051F	0000	000031	1052F	0000	000045	1053F
0000	000061	1054F	0000	000075	1055F	0000	000106	1056F	0000	000117	1057F	0000	000130	1058F
0003	R	000000	AA	0000	R	000003	ASH	0003	R	004704	BB	0000	I	000000
0000	000141	INJPS	0000	R	000001	OIL	0000	R	000002	PROT	0000	R	000004	WATER

00101	1*	SUBROUTINE WATER(TONS)												
00103	2*	COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)												
00104	3*	DO 10 I=30,32												
00107	4*	BB(I)=BB(I)*100.0												
00111	5*	PRINT 1050												
00113	6*	FORMAT(1H1//20X33H MATERIAL AND ENERGY INFORMATION ,//5X8H GFNERA												
00113	7*	CL)												
00114	8*	PRINT 1051,TONS												
00117	9*	FORMAT(/8X26H FISH												
00120	10*	OIL =TONS*BB(30)*0.01												
00121	11*	PROT =TONS*BB(31)*0.01												
00122	12*	ASH =TONS*BB(32)*0.01												
00123	13*	PRINT 1052,FB(30),OTL												
00127	14*	PRINT 1053,FB(31),PROT												
00133	15*	PRINT 1054,FB(32),ASH												
00137	16*	FORMAT(/8X10H OF WHICH ,F6.2,12H PERCENT OR,F8.3,20H - ' - IS												
00137	17*	C OIL)												
00140	18*	FORMAT(8X10H												
00140	19*	C PROTEIN)												
00141	20*	FORMAT(8X10H												
00141	21*	C ASH)												
00142	22*	PRINT 1055,AA(27,17)												
00145	23*	FORMAT(/8X26H PROCFSS STEAM												
00146	24*	WATER=AA(90,10)												
00147	25*	PRINT 1056,WATER												
00152	26*	FORMAT(/8X26H PROCESS COOLING WATER =,F8.0,7H GAL/HR)												

Table I.--Continued.

```

00153      27*      PRINT 1057,AA(90,2)
00156      28*      FORMAT(/8X26H ELECTRICITY
00157      29*      PRINT 1058
00161      30*      1058      FORMAT(///5X27H EQUIPMENT FLOW RATES
00162      31*      RETURN
00163      32*      END
END OF COMPILATION:      NO DIAGNOSTICS.

```

Table I.--Continued.

FOR,S CAPTOL,CAPTOL
FOR 59A-07/12-11:06 (0,)

SUBROUTINE CAPTOL ENTRY POINT 000411

STORAGE (USED: CODE(1) 000113; DATA(0); 000073; BLANK COMMON(2) 000000

COMMON RLOCKS:

0003 RLOCK1 005050
0004 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NPRTS
0006 NI02\$
0007 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1001F	0000	000012	1002F	0000	000021	1003F	0000	000030	1004F	0000	000037	1005F
0000	000046	1020F	0000	000055	2000F	0000	000056	2001F	0003	R	000000	AA	0003	004704
0004	000000	COST	0004	R	000007	COSTA	0000	R	000001	COSTT	0000	R	000002	DOSTT
0003	003720	IA	0000	000066	INJPS									

00101	1*													
00103	2*													
00104	3*													
00105	4*													
00106	5*	1001												
00107	6*	1002												
00110	7*	1003												
00111	8*	1004												
00112	9*	1005												
00113	10*	1020												
00114	11*	2000												
00115	12*	2001												
00117	13*													
00121	14*													
00122	15*													
00123	16*													
00126	17*													
00127	18*													
00130	19*													
00133	20*													
00134	21*													
00135	22*													
00140	23*													
00141	24*													
00142	25*													

SUBROUTINE CAPTOL (TONS)
COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
COMMON/BLOCK2/ COST(7),COSTA(7)
FORMAT(//,25X,20H EQUIPMENT ,F10.3)
FORMAT(//,25X,20H SPARE PARTS ,F10.3)
FORMAT(//,25X,20H FACILITIES ,F10.3)
FORMAT(//,25X,20H ENGINEERING ,F10.3)
FORMAT(//,25X,20H CONTINGENCIES ,F10.3,///
FORMAT(1H1)
FORMAT(20X,30H SUMMARY OF FIXED COSTS ,///
PRINT 2000
PRINT 2001
COSTTT=0.
COSTT=COSTA(5)
PRINT 1001,COSTT
COSTTT=COSTT+COSTTT
COSTT=.02*COSTA(1)
PRINT 1002,COSTT
COSTTT=COSTT+COSTTT
COSTT=AA(100,9)
PRINT 1003,COSTT
COSTTT=COSTT+COSTTT
COSTT=COSTTT*AA(98,1)
PRINT 1004, COSTT

Table I.--Continued.

```
00145      26*      COSTT=COSTT+COSTT
00146      27*      DOSTT=COSTT*AA(9R,2)
00147      28*      PRINT 1005,DOSTT
00152      29*      COSTT=DOSTT+COSTT
00153      30*      AA(100,10)=COSTT
00154      31*      PRINT 1020,AA(100,10)
00157      32*      RETURN
00160      33*      END
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

@FOR,S FASCIL,FASCIL
FOR S9A-07/12-11:06 (0,)

SUBROUTINE FASCIL ENTRY POINT 000530

STORAGE USED: CODE(1) 000536; DATA(0) 000366; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$
0005 NIQ2\$
0006 NI01\$
0007 SORT
0010 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000025	1000F	0000	000077	1010F	0000	000112	1020F	0000	000125	1030F
0000	000140	1040F	0000	000153	1050F	0000	000173	1070F	0000	000205	1080F
0000	000220	1090F	0000	000226	1100F	0000	000252	1120F	0000	000264	1130F
0000	000276	1140F	0001	000022	115G	0001	000052	140G	0001	000110	154G
0001	000123	164G	0001	000155	200G	0000	000170	210G	0001	000235	227G
0001	000250	237G	0001	000336	272G	0000	000351	302G	0001	000442	344G
0001	000455	354G	0001	000472	366G	0001	000504	90L	0003	000000	AA
0000	R 000016	ACRE	0003	R 004704	BB	0000	R 000024	BUILD	0000	R 000000	COST
0000	R 000022	DOCK	0000	R 000017	FENCEF	0003	003720	IA	0000	000354	INJPS
0000	I 000015	J	0000	T 000021	NOCK	0000	R 000020	PAVE	0000	R 000023	WARE

00101	1*	SUBROUTINE FASCIL(TONS)
00103	2*	COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104	3*	DIMENSION COST(6),COSTT(4)
00105	4*	IZ = BB(91)
00106	5*	PRINT 1000
00110	6*	1000 FORMAT(1H1//14X43H-COST OF FACILITIES AND SITE DEVELOPMENT)
00111	7*	PRINT 1001
00113	8*	1001 FORMAT(/25X85H UNIT NUMBER BASE LA
00113	9*	CBOR INDIRECT TOTAL RANGE ,/25X85H COST COSTS
00113	10*	C OF UNITS COST COSTS + OR -)
00114	11*	DO 1 J=1,6
00117	12*	COST(J) = 0.0
00120	13*	COSTT(J) = 0.0
00122	14*	ACRE=.0050*TONS
00123	15*	COST(2) = AA(99,3)*ACRE
00124	16*	COST(5) = COST(2)
00125	17*	COST(6) = COST(5)*AA(99,2)
00126	18*	PRINT 1010,AA(99,3),ACRE ,(COST(J),J=2,6)

Table I.-- Continued.

```

00136 19* 1010 FORMAT(/25H LAND ,F10.3,15H PER ACRE ,6F1
00136 C0.3)
00137 20* DO 10 J =2,6
00137 21* COST(J) = COST(J)+COSTT(J)
00142 22* FENCE = 4*SART(ACRE*0.0434)
00144 23* COST(2) = FENCE*AA(99,4)
00145 24* COST(3) = COST(2)*AA(99,5)
00146 25* COST(4) = COST(2)*AA(99,1)
00150 26* COST(5) = COST(2)+COST(3)+COST(4)
00151 27* COST(6) = COST(5)*AA(99,2)
00152 28* COST(1) = COST(5)/FFNCE
00153 29* DO 20 J=2,6
00156 30* COSTT(J)=COST(J)+COSTT(J)
00160 31* PRINT 1020,COST(1),FENCE,(COST(J),J=2,6)
00170 32* PAVE =0.333*ACRE*43.56
00171 33* COST(2) =PAVE*AA(99,6)
00172 34* COST(3) =COST(2)*AA(99,7)
00173 35* COST(4) =COST(2)*AA(99,1)
00174 36* COST(5) =COST(2)+COST(3)+COST(4)
00175 37* COST(6) = COST(5)*AA(99,2)
00176 38* COST(1) = COST(5)/PAVE
00177 39* DO 30 J=2,6
00202 40* COSTT(J) =COST(J) +COSTT(J)
00204 41* PRINT 1030,COST(1),PAVE,(COST(J),J=2,6)
00214 42* 1020 FORMAT(/25H FFNCING ,F10.3,15H PER 1000 FT ,6F1
00215 43* C0.3)
00215 44* 1030 FORMAT(/25H PAVING ,F10.3,15H PER 1.00 SQ.FT,6F1
00215 45* C0.3)
00216 46* NOCK = TONS/500. +1
00217 47* DOCK = 2.4*NOCK
00220 48* COST(2)=DOCK*AA(99,8)
00221 49* COST(3)=COST(2)*AA(99,9)
00222 50* COST(4)=COST(2)*AA(99,1)
00223 51* COST(5)=COST(2)+COST(3)+COST(4)
00224 52* COST(6)=COST(5)*AA(99,2)
00225 53* COST(1) = COST(5)/DOCK
00226 54* DO 40 J=2,6
00231 55* COSTT(J) =COST(J)+COSTT(J)
00233 56* PRINT 1040,COST(1),DOCK,(COST(J),J=2,6)
00243 57* 1040 FORMAT(/25H DOCK FACILITIES ,F10.3,15H PFR 1000 SQ.FT,6F1
00243 58* C0.3)
00244 59* PRINT 1050
00246 60* FORMAT(/25H BULK STORAGE WAREHOUSE , )
00247 61* PRINT 1060,AA(99,10)
00252 62* FORMAT( 25H ELECTRICAL WIRING ,F10.3,15H PFR 1000SQ.FT )
00253 63* PRINT 1070,AA(99,11)
00256 64* FORMAT( 25H FIRE PREVENTION EQP.,F10.3,15H PER 1000SQ.FT )
00257 65* IF (I2.EQ. 1) WARF = 0.015*TONS
00261 66* IF (I2.GT. 1) WARF = 0.003*TONS
00263 67* COST(2) =WARF*(AA(99,10)+AA(99,11))+AA(99,12)
00264 68* COST(3)=COST(2)*AA(99,13)
00265 69* COST(4)=COST(2)*AA(99,1)
00266 70* COST(5)=COST(2)+COST(3)+COST(4)
00267 71* COST(6)=COST(5)*AA(99,2)
00270 72* COST(1) = COST(5)/WARE
00271 73* DO 80 J= 2,6
00274 74* COSTT(J) =COST(J)+COSTT(J)
00274 75*

```

Table I.--Continued.

```

00276 76* PRINT 1080,COST(1),WARE,(COST(J),J=2,6)
00306 77* FORMAT(/25H TOTAL WAREHOUSE ,F10.3,15H PFR 1000 SQ.FT.,6F1
00306 78* C0.3)
00307 79* PRINT 1090
00311 80* FORMAT(/25H PROCESS BUILDING )
00312 81* PRINT 1100,AA(99,14)
00315 82* PRINT 1110,AA(99,15)
00320 83* PRINT 1120,AA(99,16)
00323 84* PRINT 1130,AA(99,17)
00326 85* FORMAT(25H ELECTRICAL WIRING ,F10.3,15H PER 1000 SQ.FT )
00327 86* FORMAT(25H HEATING AND VENTIL. ,F10.3,15H PER 1000 SQ.FT )
00330 87* FORMAT(25H PLUMBING(GENERAL) ,F10.3,15H PER 1000 SQ.FT )
00331 88* FORMAT(26H FIRE PREVENTION EQUIP,F 9.3,15HPER 1000 SQ.FT )
00332 89* BUILD =0.01*TONS
00333 90* IF(BUILD .LE. 2) RUILD = 2.0
00335 91* COST(2) =AA(99,18)*RUILD
00336 92* COST(3) =COST(2)*AA(99,19)
00337 93* COST(4) =COST(2)*AA(99,1)
00340 94* COST(5) =COST(2)+COST(3)+COST(4)
00341 95* COST(6) =COST(5)*AA(99,2)
00342 96* COST(1) = COST(5)/BUILD
00343 97* DO 140 J=2,6
00346 98* COST(J) = COST(J) +COST(J)
00350 99* PRINT 1140,COST(1),RUILD,(COST(J),J=2,6)
00360 100* FORMAT(/25H TOTAL BUILDING COSTS ,F10.3,15H PER 1000 SQ.FT.,6F1
00360 101* C0.3)
00361 102* IF(IZ .EQ. 1) GO TO 90
00363 103* COST(1) =150.
00364 104* COST(5)=COST(1)
00365 105* DO 150 J=2,6
00372 107* COST(J) = COST(J) +COST(J)
00376 108* PRINT 3012, COST(1),COST(5)
00376 109* FORMAT(/45H LABORATORY CONTROL INSTRUMENTATION ,15X,F10.
00377 110* C3,20X,F10.3)
00405 111* PRINT 2000,(COST(J),J=2,6)
00406 112* FORMAT(/25H TOTAL FACILITIES ,35XSF10.3)
00407 113* AA(100,9)=COST(5)
00410 114* RETURN
END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

OPER,S OPERAT,OPERAT
FOR 59A-07/12-11:06 (3.)

SUBROUTINE OPERAT ENTRY POINT 001242

STORAGE USED: CODE(1) 001253; DATA(0) 000757; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$
0005 NIO2\$
0006 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, REF. ACTIVE LOCATION, NAME)

0000	000127	1001F	0000	000142	1002F	0000	000155	1003F	0000	000170	1004F	0000	000203	1005F	
0000	000214	1006F	0000	000242	1007F	0000	000255	1008F	0000	000270	1009F	0001	001226	101L	
0000	000300	1010F	0000	000310	1011F	0000	000320	1012F	0000	000330	1013F	0000	000374	1018F	
0000	000407	1019F	0000	000341	1020F	0000	000327	106F	0000	000352	1104F	0000	000363	1105F	
0001	000022	114G	0000	000045	2000F	0000	000422	2001F	0000	000453	2002F	0000	000460	2003F	
0000	000467	2004F	0000	000476	2005F	0000	000505	2006F	0000	000515	2007F	0000	000524	2008F	
0000	000533	2009F	0000	000544	2010F	0000	000554	2011F	0000	000563	2012F	0000	000572	2013F	
0000	000601	2014F	0000	000610	2015F	0000	000110	2020F	0000	000117	2021F	0001	000230	3L	
0000	000666	3000F	0001	000511	330G	0001	000136	4L	0000	000617	4000F	0000	000625	4001F	
0000	000643	4002F	0001	000653	4003F	0000	000663	4005F	0000	000673	4006F	0000	000706	4007F	
0001	000233	5L	0001	000447	60L	0000	000077	6000F	0001	000565	71L	0001	000572	72L	
0001	000572	75L	0001	000572	76L	0003	R	000000	AA	0003	R	0000	000064	RYPRON	
0000	R	000052	CANS	0000	R	000053	CAST	0000	R	000000	CST	0000	R	000063	FPC
0003	003720	IA	0000	000741	INJP4	0000	I	000050	I7	0000	I	000051	J	000060	YCONC
0000	R	000054	YCOST	0000	R	000062	YHTM	0000	R	000055	YMFAL	0000	R	000057	YPAST
0000	R	000056	YSOL												

00101	1*	SUBROUTINE	OPERAT(TONS)
00101	2*	C	SUMMARY OF MATERIAL FLOW STREAMS UNDER THE INDEX AA(90,I)
00101	3*	C	1=FUEL OIL 2=POWER 3=FISH MEAL 4=FISH SOL. 5= FISH OIL
00101	4*	C	8=MAN HRS 9=CITY WATER
00101	5*	C	13=ANIOXID. 14=SU PH.ACTD
00103	6*	COMMON/BLOCK1/	AA(100,20),IA(100,5),BB(100)
00104	7*	DIMENSION	CST(20),CSTT(20)
00105	8*	I7 =	BB(91)
00106	9*	PRINT	2000
00110	10*	FORMAT(1H)	
00111	11*	PRINT	2001
00113	12*	DO 10	J=1,20
00116	13*	CST(J)=0	
00117	14*	CSTT(J)=0.0	

Table I.-- Continued.

```

00121 15*      CST(1) = TONS*BR(E)*20.0
00122 16*      PRINT 1001,TONS,CST(1)
00126 17*      CST(2) = AA(90,1)*BR(10)
00127 18*      PRINT 1002,AA(90,1),CST(2)
00133 19*      CST(3) =AA(90,2)*RB(6)*0.01
00134 20*      PRINT 1003,AA(90,2),CST(3)
00140 21*      CST(4)=AA(90,14)*BR(14)
00141 22*      IF(IZ .EQ. 1) PRINT 1004,AA(90,14),CST(4)
00146 23*      .EQ. 3) PRNT 1004,AA(90,14),CST(4)
00153 24*      IF(IZ.NE.3.AND.IZ.NE.4) GO TO 4
00155 25*      CST(16)=AA(90,17)*RB(10)
00156 26*      PRINT 3000,AA(90,17),CST(16)
00162 27*      CST(15)=AA(90,12)*RB(41)
00163 28*      3000  FORMAT(/25H 5N SODIUM HYDROXIDE ,F8.0,8H LB ,5XF8.2)
00164 29*      IF(IZ .EQ. 3) PRINT 1105,AA(90,12),CST(15)
00171 30*      IF(IZ .EQ. 4) PRINT 1105,AA(90,12),CST(15)
00176 31*      CST(14) = AA(90,15)*RB(16)
00177 32*      IF(IZ .EQ. 3) PRINT 1104,AA(90,15),CST(14)
00204 33*      IF(IZ .EQ. 4) PRINT 1104,AA(90,15),CST(14)
00211 34*      IF(IZ .EQ. 3) GO TO 3
00213 35*      IF(IZ .EQ. 4) GO TO 3
00215 36*      CST(5)=AA(90,13)*BR(13)
00216 37*      GO TO 5
00217 38*      3  CST(5)=AA(90,13)*BR(44)
00220 39*      5  CONTINUE
00221 40*      PRINT 1005,AA(90,13),CST(5)
00225 41*      CST(6)=AA(75,17)*BR(15)
00226 42*      PRINT 1006,AA(75,17),CST(6)
00232 43*      CANS=0.0
00233 44*      CANS=AA(75,4)*RB(15)
00234 45*      IF(AA(75,4).GT.0) PRINT 106,AA(75,4),CANS
00241 46*      CST(6)=CST(6)+CANS
00242 47*      CST(7) =AA(90,9)*RB(9)
00243 48*      PRINT 1007,AA(90,9),CST(7)
00247 49*      CST(8) =AA(90,8)*RB(7)
00250 50*      PRINT 1008,AA(90,8),CST(8)
00254 51*      CST(9) =AA(100,10)*RB(8)*0.1/3
00255 52*      PRINT 1009,CST(9)
00260 53*      CST(10) =AA(100,10)/30.
00261 54*      PRINT 1010,CST(10)
00264 55*      CST(11)=CST(8)*0.15
00265 56*      PRINT 1011,CST(11)
00270 57*      CST(12) =CST(10)
00271 58*      6000 FORMAT(25H BOILER WATER TREATMENT ,21XF8.2,12XF6.2,/)
00272 59*      CAST=3.3
00273 60*      PRINT 6000,CAST
00276 61*      PRINT 1012,CST(12)
00301 62*      CST(13) =CST(8)*0.30
00302 63*      PRINT 1013,CST(13)
00305 64*      IF(IZ.NE.2.AND.IZ.NF.6.AND.IZ.NE.7) GO TO 60
00307 65*      CST(18) =AA(90,18)*RB(18)
00310 66*      AA(90,18)=AA(90,18)*2000.
00311 67*      PRINT 1018,AA(90,18),CST(18)
00315 68*      CST(19) =AA(90,19) * BB(19)
00316 69*      AA(90,19)=AA(90,19)*2000.
00317 70*      PRINT 1019, AA(90,19),CST(19)
00323 71*      60  CONTINUE

```

Table I.-- Continued.

```

72* 00324 YCOST =(CST(11)+CST(12)+CST(13)+CST(14)+CST(15)+CST(16)+CST(17)+CST(18))*BB(50) +
00324 C(CST(8)+CST(9)+CST(10)+CST(11)+CST(12)+CST(13))*360.0 +(CST(14) +
73* 00324 C(CST(15)+CST(16)+CST(17)+CST(18))*BB(50)
74* 00325 YCOST=(CST(19)*BR(50)) + YCOST
75* 00326 DO 20 J=2,20
76* 00327 CST(J) =CST(J-1) + CST(J)
77* 00328 CST(J) =CST(J-1)+CST(J)
78* 00329 CST(20)=CST(20)+COST
79* 00330 PRINT 1020,CST(20)
80* 00331 PRINT 2002
81* 00332 IF (IZ.NE.2.AND.IZ.NF.6) GO TO 76
82* 00333 IF (IZ.NE.6) GO TO 71
83* 00334 FORMAT(/15X,14H HTM FISH MEAL,F8.3,10H TONS/DAY )
84* 00345 AA(90,20)=AA(90,20)/2000.
85* 00347 PRINT 2020,AA(90,20)
86* 00350 GO TO 75
87* 00351 IF (IZ.NE.2) GO TO 72
88* 00354 GO TO 75
89* 00355 GO TO 75
90* 00357 72 CONTINUE
91* 00360 76 CONTINUE
92* 00361 75 CONTINUE
93* 00362 IF (IZ
94* 00363 .EQ. 1) PRINT 2003,AA(90,3)
95* 00367 .GT. 1) PRINT 2011,AA(90,3)
96* 00373 IF (IZ .EQ. 1) PRINT 2004,AA(90,4)
97* 00377 IF (IZ.GT.2.AND.IZ.LT.6) PRINT 2012,AA(90,6)
98* 00403 IF (IZ.EQ.7) PRINT 2004,AA(90,4)
99* 00407 IF (IZ.EQ.2) PRINT 2004,AA(90,4)
100* 00413 IF (IZ .GT. 1) PRINT 2013,AA(90,7)
101* 00417 PRINT 2005,AA(90,5)
102* 00422 YMEAL = AA(90,3)*RB(50)
103* 00423 YSOL = AA(90,4)*RB(50)
104* 00424 YPAST = AA(90,6)*RB(50)
105* 00425 YCONC = AA(90,7)*RB(50)
106* 00426 YOIL = AA(90,5)*RB(50)
107* 00427 YHTM=AA(90,20)*BB(50)
108* 00430 IF (IZ.EQ.6) PRINT 2021,YHTM
109* 00434 IF (IZ .EQ. 1) PRINT 2006,YMEAL
110* 00440 IF (IZ .GT. 1) PRINT 2010,YMEAL
111* 00444 IF (IZ .EQ. 1) PRINT 2007,YSOL
112* 00450 IF (IZ.GT.2.AND.IZ.LT.6) PRINT 2014,YPAST
113* 00454 IF (IZ.EQ.2) PRINT 2007,YSOL
114* 00460 IF (IZ.EQ.7) PRINT 2007,YSOL
115* 00464 IF (IZ .GT. 1) PRINT 2015,YCONC
116* 00470 FORMAT(/15X 14H HTM FISH MEAL,F8.0,11H TONS/YEAR )
117* 00471 PRINT 2008,YOIL
118* 00474 PRINT 2009,YCOST
119* 00477 FORMAT(/25H FISH
120* C.2)
121* 00500 1001 FORMAT(/25H FUEL OIL ,F8.0,8H TONS .5XF8.2,12XF6
122* C.2)
123* 00501 1002 FORMAT(/25H FUEL OIL ,F8.0,8H GALLONS,5XF8.2,12XF6
124* C.2)
125* 00502 1003 FORMAT(/25H ELECTRICITY ,F8.0,8H KWHR .5XF8.2,12XF6
126* C.2)
127* 00503 1004 FORMAT(/25H SULPHURIC ACID ,F8.0,8H LB ,5XF8.2,12XF6
128* 00504 1005 FORMAT(/25H ANTIOXIDANT ,F8.0,8H BAGS ,5XF8.2,12XF6
1006 FORMAT(/25H PACKAGING

```

Table I.- Continued.

00504	129*	C2)							
00505	130*	106	FORMAT(/25H PACKAGING					,F8.0,8H CANS	,5XF8.2,12XF6.
00505	131*	C2)							
00506	132*	1007	FORMAT(/25H CITY WATER						,F8.0,8H GALLONS.5XF8.2,12XF6
00506	133*	C.2)							
00507	134*	1008	FORMAT(/25H LABOR AND SUPERVISION						,F8.0,8H MAN HR.5XF8.2,12XF6
00507	135*	C.2,/))							
00510	136*	1009	FORMAT(/25H DEPRECIATION						,21XF8.2,12XF6.2)
00511	137*	1010	FORMAT(/25H MAINTENANCE						,21XF8.2,12XF6.2)
00512	138*	1011	FORMAT(/25H PAYROLL EXTRAS						,21XF8.2,12XF6.2)
00513	139*	1012	FORMAT(/25H INSURANCE AND TAXES						,21XF8.2,12XF6.2)
00514	140*	1013	FORMAT(/25H OVERHEAD						,21XF8.2,12XF6.2,/))
00515	141*	1020	FORMAT(/25H TOTAL OPERATING COSTS						,21XF8.2,12XF6.2,/))
00516	142*	1104	FORMAT(/25H CALCIUM HYDROXIDE						,F8.0,8H LB .5XF8.2)
00517	143*	1105	FORMAT(/25H ENZYME						,F8.0,8H LB .5XF8.2)
00520	144*	1018	FORMAT(/25H ISOPROPYL ALCOHOL						,F8.0,8H POUNDS .5XF8.2,12XF6
00520	145*	C.2)							
00521	146*	1019	FORMAT(/25H PHOSPHORIC ACID						,F8.0,8H POUNDS .5XF8.2,12XF6
00521	147*	C.2)							
00522	148*	2001	FORMAT(20X,17H OPERATING COSTS						,/75H COST ITFM
00522	149*	CQUANTITY USED	COST IN DOLLARS						,/43X30H PER D
00522	150*	CAY							
00523	151*	2002	FORMAT(/20X,17H PRODUCTION RATE)						
00524	152*	2003	FORMAT(/15X12H FISH MEAL						,F10.3,10H TONS/DAY)
00525	153*	2004	FORMAT(/15X12H FISH SOL.						,F10.3,10H TONS/DAY)
00525	154*	C							
00526	155*	2005	FORMAT(/15X12H FISH OIL						,F10.3,10H TONS/DAY)
00527	156*	2006	FORMAT(/15X12H FISH MEAL						,F10.0,11H TONS/YEAR)
00530	157*	2007	FORMAT(/15X 12H FISH SOL.						,F10.0,11H TONS/YEAR)
00531	158*	2008	FORMAT(/15X 12H FISH OIL						,F10.0,11H TONS/YEAR)
00532	159*	2009	FORMAT(/20X24H YEARLY OPERATING COST						=,F12.6,8H DOLLARS)
00533	160*	2010	FORMAT(/15X12H BONE MEAL						,F10.0,11H TONS/YEAR)
00534	161*	2011	FORMAT(/15X12H BONE MEAL						,F10.3,10H TONS/DAY)
00535	162*	2012	FORMAT(/15X12H FISH PASTE						,F10.3,10H TONS/DAY)
00536	163*	2013	FORMAT(/15X12H DRY CONC.						,F10.3,10H TONS/DAY)
00537	164*	2014	FORMAT(/15X 12H FISH PASTE						,F10.0,11H TONS/YEAR)
00540	165*	2015	FORMAT(/15X 12H Dry CONC.						,F10.0,11H TONS/YEAR)
00541	166*	IF (IZ.EQ. 1) GO TO 101							
00543	167*	PRINT 4000							
00545	168*	4000	FORMAT(/20X,24H PRODUCTION COST OF FPC)						
00546	169*	PRINT 4001							
00550	170*	4001	FORMAT(74H BY-PRODUCT						PRICE(CENTS/POUND)
00550	171*	CRTH(DOLLARS/YEAR))							TOTAL WO
00551	172*	YMEAL=YMEAL*2000.*RB(66)/100.							
00552	173*	IF (YMEAL.GT.0) PRINT 4002.RB(66),YMEAL							,F8.1,13XE12.6)
00557	174*	FORMAT(/25H BONE MEAL							
00560	175*	Y0IL=Y0IL*2000.*BB(67)/100.							
00561	176*	PRINT 4003.BR(67),Y0TL							
00565	177*	FORMAT(/25H FISH OIL							,F8.1,13XF12.6)
00566	178*	YSOL=YSOL*2000.*BB(68)/100.							
00567	179*	IF (17.EQ.2.Or.12.EQ.7) PRINT 4005.RB(68),Y50I							,F8.1,13XF12.6)
00574	180*	FORMAT(/25H FISH SOLUBLES							
00575	181*	YCONC=YCONC*2000.*.5n*YPACT*2000.							
00576	182*	FPC=(YCONC/YCONC)*100.							
00577	183*	PRINT 4006.FPC							
00602	184*	4006	FORMAT(/20X,32H FPC COST WITHOUT BY-PRODUCTS						,F8.1,13H CENTS/POU
00602	185*	CND)							

Table I.-- Continued.

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00603      186*      BYPROD=YOIL+YSOL+YMEAL+YPAST
00604      187*      YCOST=YCOST-RYPROD
00605      188*      FPC=(YCOST/YCONC)*100.
00606      189*      PRINT 4007,FPC
00611      190*      4007 FORMAT(/20X,32H FPC COST WITH RY-PRODUCTS      ,F8.1,13H CENTS/POU
00612      191*      CND )
00613      192*      101 RETURN
00613      193*      END

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END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S LIBRF,LIBRE
FOR S9A-07/12-11:06 (1,)

SUBROUTINE LIBRE ENTRY POINT 001n77

STORAGE USED: CODE(1) 001106; DATA(0) 000247; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 DATA1 000050
0004 RLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0004 R 000000 AA 0004 R 0047n4 BB 0003 R 000000 DATB 0004 003720 IA 0000 000230 INJPS

00101	1*	SUBROUTINE LIBRE						
00103	2*	COMMON/ DATA1 / DATR(8,5)						
00104	3*	COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)						
00104	4*	C IDENTIFICATION OF DATA STORED IN LIBRARY SUBROUTINE						
00104	5*	C						
00104	6*	C EQUIPMENT INDEX NUMBERS						
00104	7*	C						
00104	8*	C						
00104	9*	C						
00104	10*	C						
00104	11*	C						
00104	12*	C						
00104	13*	C						
00104	14*	C						
00104	15*	C						
00104	16*	C						
00104	17*	C						
00104	18*	C						
00104	19*	C						
00104	20*	C						
00104	21*	C						
00104	22*	C						
00104	23*	C						
00104	24*	C						
00104	25*	C						
00104	26*	C						
00104	27*	C						
00104	28*	C						
00104	29*	C						
00104	30*	C						

Table I.--Continued.

00104	31*	C	66= CENTRIFUGAL PUMPS	CALLED BY SUB.	PMPCNT
00104	32*	C	67= SHELL-TUBE HEAT EXCHANGERS	CALLED BY SUB.	HEATEX
00104	33*	C	70= BELT CONVEYER	CALLED BY SUB.	BELT
00104	34*	C	71= BUCKET CONVEYFR	CALLED BY SUB.	BUCKET
00104	35*	C	72= SCALE	CALLED BY SUB.	SCALE
00104	36*	C	73= AGITATOR-PROPELLAR	CALLED BY SUB.	AGITOR
00104	37*	C	74= BALL MILL	CALLED BY SUB.	BALMII
00104	38*	C	75= BAGGING MACHINE	CALLED BY SUB.	BAGGMA
00104	39*	C	78= ROTARY DRUM FILTER	CALLED BY SUB.	FILTER
00104	40*	C	80= OVERHEAD CRANE	CALLED BY SUB.	CRANES
00104	41*	C	81= URAG CONVEYFR	CALLED BY SUB.	DRAGMA
00104	42*	C	85= MECHANICAL REFRIGERATION	CALLED BY SUB.	REFRIG
00104	43*	C	99= FACILITIES	CALLED BY SUB.	FASCII
00104	44*	C			
00104	45*	C	GENERAL IDENTIFICATION OF THE STORED DATA.		
00104	46*	C	THE FOLLOWING DATA WILL IN MOST CASES BE STORED UNDER THE IDENTIF-		
00104	47*	C	YING INDEX NUMBER FOR EACH IDOM OF EQUIPMENT. VARIATIONS OR ADDI-		
00104	48*	C	TIONS TO THIS PATTERN ARE EXPLAINED UNDER THE RESPECTIVE HEADINGS.		
00104	49*	C			
00104	50*	C	AA(IX,7) = UNIT COST		
00104	51*	C	AA(IX,8) = EXPONENT OF COST EQUATION		
00104	52*	C	AA(IX,11) = FIELD MATERIALS COST FACTOR		
00104	53*	C	AA(IX,12) = DIRECT LABOR COST FACTOR		
00104	54*	C	AA(IX,13) = INDIRECT COST FACTOR		
00104	55*	C	AA(IX,15) = UNCERTAINTY FACTOR FOR BARE MODULE COST		
00104	56*	C			
00104	57*	C	CONICAL HOPPERS. SIZE UNIT CURTIC FEET. REF GUTHRIE		
00105	58*	C	AA(6,7) = 0.010		
00106	59*	C	AA(6,8) = 0.68		
00107	60*	C	AA(6,11) = 0.04		
00110	61*	C	AA(6,12) = 0.01		
00111	62*	C	AA(6,13) = 0.42		
00112	63*	C	AA(6,15) = 0.10		
00113	64*	C	AA(6,18) = 2.40		
00113	65*	C	FISH STORAGE		
00114	66*	C	AA(7,7) = 0.0		
00115	67*	C	AA(7,8) = 0.9		
00116	68*	C	AA(7,11) = 0.0		
00117	69*	C	AA(7,12) = 0.10		
00120	70*	C	AA(7,13) = 4		
00121	71*	C	AA(7,15) = 0.1		
00121	72*	C	BAROMETRIC CONDENSER AND SCRUBBERS		
00122	73*	C	AA(8,7) = 20.		
00123	74*	C	AA(8,8) = 1.0		
00124	75*	C	AA(8,11) = 0.33		
00125	76*	C	AA(8,12) = 0.33		
00126	77*	C	AA(8,13) = 0.33		
00127	78*	C	AA(8,15) = 0.1		
00127	79*	C	PULVERIZER		
00130	80*	C	AA(11, 7) = 520.		
00131	81*	C	AA(11, 8) = .35		
00132	82*	C	AA(11,11) = .272		
00133	83*	C	AA(11,12) = .318		
00134	84*	C	AA(11,13) = .4		
00135	85*	C	AA(11,15) = .1		
00135	86*	C	SCREW CONVEYER		
00136	87*	C	AA(17, 7) = 1000.0		

Table I.--Continued.

00137	88*	AA(17, 8) =	.9
00140	89*	AA(17, 11) =	.272
00141	90*	AA(17, 12) =	.318
00142	91*	AA(17, 13) =	.4
00143	92*	AA(17, 15) =	.1
00143	93*	C HAMMER MILL SIZE + COST DATA, REF GUTHRIE	
00143	94*	C SIZE UNIT = TON PER HOUR	
00144	95*	AA(18, 7) =	0.5
00145	96*	AA(18, 8) =	0.45
00146	97*	AA(18, 11) =	0.27
00147	98*	AA(18, 12) =	0.431
00150	99*	AA(18, 13) =	0.44
00151	100*	AA(18, 15) =	0.10
00151	101*	C DRUM DRYER	
00152	102*	AA(19, 7) =	3000.
00153	103*	AA(19, 8) =	.38
00154	104*	AA(19, 11) =	.279
00155	105*	AA(19, 12) =	.461
00156	106*	AA(19, 13) =	.4
00157	107*	AA(19, 15) =	.1
00157	108*	C PAN DRYER	
00160	109*	AA(20, 7) =	1900.
00161	110*	AA(20, 8) =	.38
00162	111*	AA(20, 11) =	.279
00163	112*	AA(20, 12) =	.461
00164	113*	AA(20, 13) =	.4
00165	114*	AA(20, 15) =	.1
00165	115*	C ROTARY VACUUM DRYER	
00166	116*	AA(21, 7) =	2500.
00167	117*	AA(21, 8) =	.45
00170	118*	AA(21, 11) =	.279
00171	119*	AA(21, 12) =	.20
00172	120*	AA(21, 13) =	.16
00173	121*	AA(21, 15) =	.1
00173	122*	C BOILER	
00174	123*	AA(27, 7) =	395.5
00175	124*	AA(27, 8) =	.5
00176	125*	AA(27, 11) =	.19
00177	126*	AA(27, 12) =	.15
00200	127*	AA(27, 13) =	.2
00201	128*	AA(27, 15) =	.1
00201	129*	C SPRAY EVAPORATOR SIZE UNIT = LB OF WATER EVAP. PER HR	
00201	130*	C PRAY AND FILM EVAP. INCLUIDE SCRUBBERS AND BAR. CONDENSRS. BASE	
00201	131*	C COST FROM CHEM. FNG. FEB. 9, 1970, OTHER FACTORS EQ. TO EVAP. FROM	
00201	132*	C GUTHRIE	
00202	133*	AA(30, 7) =	0.050
00203	134*	AA(30, 8) =	1.0
00204	135*	AA(30, 11) =	0.66
00205	136*	AA(30, 12) =	0.24
00206	137*	AA(30, 13) =	0.42
00207	138*	AA(30, 15) =	0.10
00207	139*	C WIPE FILM EVAPORATORS SIZE UNIT = SQ. FT AREA	
00210	140*	AA(31, 7) =	0.9
00211	141*	AA(31, 8) =	0.31
00212	142*	AA(31, 11) =	0.66
00213	143*	AA(31, 12) =	0.24
00214	144*	AA(31, 13) =	0.42

Table I.--Continued.

nn215	145*	AA(31,15) = 0.10
nn216	146*	C FORCED CIRCULATION EVAPORATORS SIZE UNIT= 50 FT REF GUTHRIE
nn217	147*	AA(32,7)=0.6
nn218	148*	AA(32,8) = 0.70
nn219	149*	AA(32,11) = 0.66
nn220	150*	AA(32,12) = 0.24
nn221	151*	AA(32,13) = 0.42
nn222	152*	AA(32,15) = 0.10
nn223	153*	AA(32,18) = 2.40
nn224	154*	C VERTICAL EVAPORATORS SIZE UNIT = 50. FT. REF. GUTHRIE
nn225	155*	AA(33,7) = 0.12
nn226	156*	AA(33,8) = 0.53
nn227	157*	AA(33,11) = 0.66
nn228	158*	AA(33,12) = 0.24
nn229	159*	AA(33,13) = 0.42
nn230	160*	AA(33,15) = 0.10
nn231	161*	AA(33,18) = 2.40
nn232	162*	C STORAGE TANK SIZE AND COST DATA. REF GUTHRIE
nn233	163*	C SIZE UNITS 100 GAL CAPACITY . MATERIAL FACTOR INDEX 18 = SST
nn234	164*	AA(40,7) = 0.88
nn235	165*	AA(40,8) = 0.31
nn236	166*	AA(40,11) = 0.20
nn237	167*	AA(40,12) = 0.27
nn238	168*	AA(40,13) = 0.49
nn239	169*	AA(40,15) = 0.10
nn240	170*	AA(40,18) = 3.2
nn241	171*	C STORAGE TANK FROM 1000 GAL TO 40000 GAL CAPACITY STEFL + SST REF GUT
nn242	172*	C HRIE. SIZE UNITS 100-DC GAL
nn243	173*	AA(41,7) = 0.5
nn244	174*	AA(41,8) = 0.35
nn245	175*	AA(41,11) = 0.38
nn246	176*	AA(41,12) = 0.10
nn247	177*	AA(41,13) = 0.49
nn248	178*	AA(41,15) = 0.10
nn249	179*	AA(41,18) = 3.2
nn250	180*	C PRESSURE VESSEL
nn251	181*	C FOR THE PRESSURE VESSEL(TA(42,3) DETERMINES THE METAL,IA(42,2) = 1
nn252	182*	C IMPLIES VERTICAL CONSTRUCTION(AA(42,18) IS THE DIAMETER,AA(42,19)
nn253	183*	C IS THE HEIGHT
nn254	184*	AA(42, 1)= 3.67
nn255	185*	AA(42, 2)= 2.25
nn256	186*	AA(42, 3)= 1.0
nn257	187*	AA(42,15)= .1
nn258	188*	C DISTILLATION COLUMN
nn259	189*	C THE METAL,AA(43,20) THE WIDTH,AA(43,18) THE TRAY SEPARATION,
nn260	190*	C AA(43,17) THE HEIGHT
nn261	191*	C DETERMINES THE WIDTH
nn262	192*	AA(43, 4)= 0.4
nn263	193*	AA(43, 5)= 1.8
nn264	194*	AA(43,15)= .1
nn265	195*	AA(43,1)= 1.7
nn266	196*	AA(43,8) =1.0
nn267	197*	AA(43,11)= .3
nn268	198*	AA(43,12)= .4
nn269	199*	AA(43,13)= .4
nn270	200*	AA(43,15)= .1
nn271	201*	C JACKETED REACTOR VFSSEI UNIT COST 3*TANK COST DATA GUTHRIE. SI7F=6AL

Table I.-- Continued.

00267	AA(49,7) = 0.240
00270	AA(49,8) = 0.35
00271	AA(49,11) = 0.38
00272	AA(49,12) = 0.10
00273	AA(49,13) = 0.49
00274	AA(49,15) = 0.10
00275	AA(49,18) = 3.20
00275	C FISH GRINDER BASED ON 3 TON/HR UNIT COST OF 18300 DOLLARS. OTHER FAC-
00275	C TORS AS FOR BALL MILL
00276	AA(50,7) = 2.54
00277	AA(50,8) = 0.65
00300	AA(50,11) = 0.54
00301	AA(50,12) = 0.195
00302	AA(50,13) = 0.42
00303	AA(50,15) = 0.10
00304	AA(50,18) = 2.4
00305	C VIBRATING SCREEN FILTERS. SINGLE. SIZE UNIT = SURFACE AREA. REF GIITH.
00305	AA(51,7) = 0.7
00306	AA(51,8) = 0.58
00307	AA(51,11) = 0.27
00310	AA(51,12) = 0.05
00311	AA(51,13) = 0.42
00312	AA(51,15) = 0.10
00313	AA(51,18) = 2.40
00313	C SHARPLES CENTRIFUGE
00314	AA(52,7)=5200.
00315	AA(52, 8)= .68
00316	AA(52,11)= .26
00317	AA(52,12)= .34
00320	AA(52,13)= .4
00321	AA(52,15)= .1
00321	C SOLID BOWL CENTRIFUGE
00322	AA(53, 7)= 1900.
00323	AA(53,8)= .73
00324	AA(53,11)= .26
00325	AA(53,12)= .34
00326	AA(53,13)= .4
00327	AA(53,15)= .1
00327	C VERTICAL BASKET CENTRIFUGE
00330	AA(54, 7)= 620.
00331	AA(54, 8)= 1.
00332	AA(54,11)= .26
00333	AA(54,12)= .194
00334	AA(54,13)= .4
00335	AA(54,15)= .1
00335	C FLOWING SOLIDS BLENDER
00335	C A COST OF 15000 FOR 750 FT**3/HR UNIT NORMALIZED TO GTVE
00336	AA(57,7) = 0.47
00337	AA(57,8) = 0.52
00340	AA(57,11) = 0.48
00341	AA(57,12) = 0.13
00342	AA(57,13) = 0.42
00343	AA(57,15) = 0.10
00343	C CENTRIFUGAL AND RECD. PUMPS ARE COST FITED BY A QUADRATIC EQ. IN TERMS
00343	C OF LOG(SIZE). (REF. GUTHRIE) SIZE UNIT = GPM*PSI. THE EQ IS:
00343	C LOG(COST)= LOG(UNIT COST) + EXP*LOG(SIZE) + BEXP*LOG(SIZE)**2
00343	C UNIT COST = AA(IX,7) EXP = AA(IX,8) BEXP=AA(IX,9)
00343	258*

Table I.-- Continued.

00343	C	259*	
00343	C	260*	C CENTRIFUGAL PUMPS. MATERIAL FACTOR IA(66,1)=0/1/2 =FE/BRONZE/SST
00343	C	261*	AA(66,18)=BRONZF FACTOR, AA(66,19)= SST FACTOR
00344		262*	AA(66,7) =0.5
00345		263*	AA(66,8) =0.174
00346		264*	AA(66,9) =0.049
00347		265*	AA(66,11) =0.71
00350		266*	AA(66,12) =0.35
00351		267*	AA(66,13) =0.44
00352		268*	AA(66,15) =0.10
00353		269*	AA(66,18) = 1.28
00354		270*	AA(66,19) = 1.93
00355	C	271*	C RECIPROCATING PUMPS. SAME AS FO CFNTRIFUGAL (REF GUTHRIE)
00356		272*	AA(65,7) = 3.2
00357		273*	AA(65,8) = 0.281
00360		274*	AA(65,9) = 0.0335
00361		275*	AA(65,11) = 0.71
00362		276*	AA(65,12) = 0.70
00363		277*	AA(65,13) = 0.89
00364		278*	AA(65,15) = 0.10
00365		279*	AA(65,18) = 1.25
00366		280*	AA(65,19) = 2.10
00367		281*	C COST AND SIZE VALUES FOR SHELL-TUBE HEAT EXCHANGERS. REF GUTHRIE
00370		282*	C SIZE UNITS ARE SQ. FT OF SURFACE AREA
00371		283*	AA(67,7) = 0.113
00372		284*	AA(67,8) = 0.622
00373		285*	AA(67,11) = 0.714
00374		286*	AA(67,12) = 0.63
00375		287*	AA(67,13) = 0.947
00376		288*	AA(67,15) = 0.17
00377		289*	C MATERIAL FACTORS FOR HEAT EXCHANGERS. SHELL/TUBE. INDEX 1A = ST/SST
00400		290*	C INDEX 19 = SST/SST REF GUTHRIE
00401		291*	AA(67,18) = 2.25
00402		292*	AA(67,19) = 3.26
00403		293*	C BELT CONVEYER
00404		294*	AA(70, 7)= 540.
00405		295*	AA(70, 8)= .65
00406		296*	AA(70,11)= .27
00407		297*	AA(70,12)= .39
00408		298*	AA(70,13)= .4
00409		299*	AA(70,15)= .1
00410		300*	C BUCKET CONVEYER
00411		301*	AA(71, 7)= 220.
00412		302*	AA(71, 8)= .65
00413		303*	AA(71,11)= .278
00414		304*	AA(71,12)= .562
00415		305*	AA(71,13)= .4
00416		306*	AA(71,15)= .1
00417		307*	C SCALE
00418		308*	AA(72,20)= 4.0
00419		309*	AA(72,18)= 7.2
00420		310*	AA(72,19)= 8.55
		311*	AA(72,11)=0.08
		312*	AA(72,13)=0.4
		313*	AA(72,15)= 0.1
		314*	C AGITATOR
		315*	AA(73, 7)= 350.

Table I.--Continued.

00421	316*	AA(73, 8) = .5
00422	317*	AA(73,11) = .276
00423	318*	AA(73,12) = .344
00424	319*	AA(73,13) = .4
00425	320*	AA(73,15) = .1
00426	321*	C BALL MILL COST DATA, MATFRIAL FACTOR INDEX=18, SIF TONS/HR REF GUTHRIF
00427	322*	AA(74,7) = 0.55
00428	323*	AA(74,8) = 0.65
00429	324*	AA(74,11) = 0.54
00431	325*	AA(74,12) = 0.195
00432	326*	AA(74,13) = 0.42
00433	327*	AA(74,15) = 0.10
00434	328*	AA(74,18) = 2.4
00434	329*	C BAGGING MACHINE
00435	330*	AA(75,7)=3300.
00436	331*	AA(75,8)=0.8
00437	332*	AA(75,11)=.40
00440	333*	AA(75,12)=0.11
00441	334*	AA(75,13)= .4
00442	335*	AA(75,15)=.1
00443	336*	AA(75,1)=1000.
00443	337*	C ROTARY DRUM FILTERS, SIZE UNITS SQ.FT. SURFACE REF GUTHRIF
00444	338*	AA(78,7) = 1.40
00445	339*	AA(78,8) = 0.63
00446	340*	AA(78,11) = 0.47
00447	341*	AA(78,12) = 0.13
00450	342*	AA(78,13) = 0.42
00451	343*	AA(78,15) = 0.10
00452	344*	AA(78,18) = 2.4
00452	345*	C OVERHEAD CRANES, IA(80,1)= INDEX FOR SPAN 0=20FT;1=30FT;2=40FT, SPAN
00452	346*	C UNIT SIZE FACTORS ARE AA(80,18)=30FT ; AA(80,19)=40FT .SIZE UNITS=TONS
00453	347*	AA(80,7) =1.2
00454	348*	AA(80,8) =0.60
00455	349*	AA(80,11) = 0.46
00456	350*	AA(80,12) = 0.12
00457	351*	AA(80,13) = 0.42
00460	352*	AA(80,15) = 0.10
00461	353*	AA(80,18) = 1.6
00462	354*	AA(80,19) = 2.0
00462	355*	C DRAG CONVEYER
00463	356*	AA(81,7)=9.
00464	357*	AA(81,8)=.8
00465	358*	AA(81,13) =.4
00466	359*	AA(81,15)= .1
00466	360*	C MECHANICAL REFRIGRATION, SIZE UNITS= TONS.
00466	361*	C COOLING TEMP. INDEX = IA(85,1) WHICH SHOULD CONTAIN TEMP. IN DEG F
00466	362*	C AA(85,18) THEN CONTAINS FACTOR FOR 20 AA(85,19) FOR 0 DEG
00467	363*	AA(85,7) =2.9
00470	364*	AA(85,8) = 0.70
00471	365*	AA(85,11) =0.17
00472	366*	AA(85,12) =0.14
00473	367*	AA(85,13) =0.11
00474	368*	AA(85,15) =0.10
00475	369*	AA(85,18) =1.95
00476	370*	AA(85,19) =2.25
00476	371*	C COST OF FACILITIES INDE= 99 DETAIL INDEX IDENTIFIES SEP. IDOMS
00476	372*	C I= FACILITIES,INDIRECTS P=FACILITIES CERTAINTY RANGE 3=COST OF LAND

Table I.-- Continued.

00474	373*	C PER ACRE 4=COST OF FENCF/1000 FT 5=LABOR FACTOR FENCF 6 = COST OF PAV
00476	374*	C MENT/1000 FT**2 7=LABOR FACTOR PAVEMENT 8= COST OF DOCK 9=COST OF CO
00476	375*	C STRUCT LABOR , 10=WAREHOUSE LIGHTING COST/1000FTSQ 11= WAREH. FIR PRE
00476	376*	C VENTION COST 12= WAREH. BASE SHELL COST 13= CONST. LABOR FACTOR 14=LI
00476	377*	C GHING 15=HEAT AND VENT. 16= PUMRING 17=FIPEVENTION 18=RASE 19-LABOR
00477	378*	AA(98,2)=.10
00500	379*	AA(98,1)=0.075
00501	380*	AA(99,1) = 0.34
00502	381*	AA(99,2) = 0.15
00503	382*	AA(99,3)=10.0
00504	383*	AA(99,4) = 1.61
00505	384*	AA(99,5) = 0.32
00506	385*	AA(99,6) = 0.364
00507	386*	AA(99,7) = 1.75
00510	387*	AA(99,8) = 0.65
00511	388*	AA(99,9) = 2.50
00512	389*	AA(99,10) =0.90
00513	390*	AA(99,11) =1.10
00514	391*	AA(99,12) =3.22
00515	392*	AA(99,13) =0.34
00516	393*	AA(99,14) =1.75
00517	394*	AA(99,15) =1.50
00520	395*	AA(99,16) =1.70
00521	396*	AA(99,17) =1.10
00522	397*	AA(99,18) =8.80
00523	398*	AA(99,19) =0.34
00524	399*	AA(99,20) = 15.
00525	400*	AA(100,1)=3.
00526	401*	AA(100,2)=32.
00527	402*	AA(100,3)= 1.125 E-02
00530	403*	AA(100,4)= 5.00
00531	404*	AA(100,7)= 5.0E-05
00532	405*	AA(100,8) = 1.3 E-05
00533	406*	AA(100,9) = 1.E-07
00534	407*	AA(100,11)=.724
00535	408*	AA(100,12) = .074
00536	409*	AA(100,13)=0.1
00537	410*	AA(100,20) = 20.
00537	411*	C THE BB(I) COMMON BLOCK INCLUDES BUILT IN PRICE SCHEDULES.
00537	412*	C 9=CITY WATER 10=FUEL OIL 13=ANTIOXIDANT 14=SULPHURIC ACID 15=FISH MEA
00537	413*	C L BAGS 16=CAOH 66=PRICE OF BONE MEAL (CENTS/LB) 67=PRICE OF FISH OIL
00537	414*	C (CENTS/LB) 68=PRICE OF FISH SOLUBLES(CENTS/LB)
00540	415*	BB(9)=.25*.001
00541	416*	BB(10)=.06
00542	417*	BB(13)=4.00
00543	418*	BB(14)=.017
00544	419*	BB(15) = 0.25
00545	420*	BB(16) = 0.01
00546	421*	BB(18)=129.22
00547	422*	BB(66)=3.5
00550	423*	BB(67)=4.0
00551	424*	BB(68)=3.5
00552	425*	BB(19)=45.
00552	426*	
00552	427*	C DATA FOR ISOPROPYL EXTRACTION (FRACTION OF STREAM EXTRACFD IN STAGE)
00552	428*	C DATB(STAGE,STREAM) STRFAM INDICES 1-OIL 2-PROTEIN 3-ASH 4-WATER
00552	429*	C 5-ISOPROPYL ALCOHOL

Table I.-- Continued.

```

00552      C
00553      430*      DATB(1,1)= 28./148.
00554      431*      DATR(2,1)= 8./24.
00555      432*      DATB(3,1)= 4./8.
00556      433*      DATB(4,1)= 1./4.
00557      434*      DATB(5,1)= 1./4.
00558      435*      DATB(6,1)= 1./4.
00559      436*      DATB(7,1)= 1./4.
00560      437*      DATB(8,1)= 1./4.
00561      438*      DATR(1,2)= 487./605.
00562      439*      DATR(2,2)= 477./487.
00563      440*      DATB(3,2)= 476./477.
00564      441*      DATB(4,2)= 471./476.
00565      442*      DATB(5,2)= 471./476.
00566      443*      DATB(6,2)= 471./476.
00567      444*      DATB(7,2)= 471./476.
00568      445*      DATB(8,2)= 471./476.
00569      446*      DATB(1,3)= 100./124.
00570      447*      DATR(2,3)= 98./110.
00571      448*      DATB(3,3)= 97./98.
00572      449*      DATB(4,3)= 96./97.
00573      450*      DATR(5,3)= 96./97.
00574      451*      DATB(6,3)= 96./97.
00575      452*      DATB(7,3)= 96./97.
00576      453*      DATB(8,3)= 96./97.
00577      454*      DATR(1,4)= (963.+(-123*125.))/3276.
00578      455*      DATB(2,4)= (543.+(-123*161.))/(963.+(-123*125.))
00579      456*      DATR(3,4)= (324.+(-123*301.))/(543.+(-123*161.))
00580      457*      DATB(4,4)= (38.+(-123*553.))/(324.+(-123*301.))
00581      458*      DATB(5,4)= NATB(4,4)
00582      459*      DATB(6,4)= NATB(5,4)
00583      460*      DATB(7,4)= NATB(6,4)
00584      461*      DATB(8,4)= NATB(7,4)
00585      462*      DATR(1,5)= 125.*.R77 / 3276.
00586      463*      DATR(2,5)= 161./125.
00587      464*      DATB(3,5)= 301./161.
00588      465*      DATB(4,5)= 553./301.
00589      466*      DATB(5,5)= NATB(4,5)
00590      467*      DATB(6,5)= NATB(5,5)
00591      468*      DATB(7,5)= NATB(6,5)
00592      469*      DATB(8,5)= NATB(7,5)
00593      470*      RETURN
00594      471*      END
00595      472*

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

MAP
MAP 22B -07-12-11:06

ADDRESS LIMITS 001000 043715 044000 071006
STARTING ADDRESS 043307

WORDS DECIMAL 17870 IBANK 10750 DBANK

	SEGMENT	MAIN	001000	043715	044000	071006
NSWTS\$/FOR	1	001000	001021			
NWBLK\$/FOR	1	001022	001164	0	044000	044006
NFTCH\$/FOR	1	001165	001524	2	044007	044061
FxP\$/FOR	1	001525	001614	2	044062	044102
NTOC\$/FOR	1	001615	001174	2	044103	046602
NOS\$/FOR	1	003175	004263	2	046603	046673
NITABS\$/FOR				2	046674	046732
NERRSD/UOM				0	046733	047000
FRUS						
NTB\$/FOR	1	004264	004556	2	047001	047022
UOMSYS (COMMON BLOCK)				2	047023	047037
HMONITOR/RALPH	1	004557	004606	2	047040	047677
				4	UOMSYS	
NTS\$/FOR	1	006007	007132	2	047700	047751
AI 06\$/FOR	1	007133	007251	2	047752	050012
NFXP\$/FOR	1	007252	007325	2	050013	050022
SORT\$/FOR	1	007326	007366	2	050023	050034
NTOS\$/FOR	1	007367	011022	2	050035	050417
NOSYMS\$/FOR	1	011023	011261	2	050420	050431
NRRS/UOM	1	011262	011742	2	050432	050604
BI OCK4 (COMMON BLOCK)					050605	050616
BI OCK2 (COMMON BLOCK)					050617	050634
BI OCK1 (COMMON BLOCK)					050635	055704
DATA1 (COMMON BLOCK)					055705	055754
BI ANK\$COMMON (COMMON BLOCK)						
LIBRE	1	011743	013050	0	057555	056223
	3	DATA1		2	BI ANK\$COMMON	
OPERAT	1	013051	014323	4	BLOCK1	
	2	BLOCK1		0	056224	057202
FASCIL	1	014324	015061	2	PLANK\$COMMON	
	3	BLOCK1		0	057203	057567
CAPTOL	1	015062	015174	2	PLANK\$COMMON	
	3	BLOCK1		0	057570	057662
				4	PLANK\$COMMON	
				4	BLOCK2	
MAITP	1	015175	015315	0	057663	060033
	3	BLOCK1		2	BI ANK\$COMMON	
RFRTRG	1	015316	015442	0	060034	060044

Table I.--Continued.

DRAGMA	3	BLOCK1			2	BLANK&COMMON
	1	015443	015613		4	BLOCK2
	3	BLOCK1			0	060065 060135
CRANFS					2	BLANK&COMMON
	1	015614	015741		4	BLOCK2
	3	BLOCK1			0	060135 060220
FILTER					2	BLANK&COMMON
	1	015762	016060		4	BLOCK2
	3	BLOCK1			0	060221 060251
BAGGMA					2	BLANK&COMMON
	1	016061	016212		4	BLOCK2
	3	BLOCK1			0	060252 060322
BALMIL					2	BLANK&COMMON
	1	016213	016311		4	BLOCK2
	3	BLOCK1			0	060323 060353
AGITOR					2	BLANK&COMMON
	1	016312	016411		4	BLOCK2
	3	BLOCK1			0	060354 060406
SCAF					2	BLANK&COMMON
	1	016412	016544		4	BLOCK2
	3	BLOCK1			0	060407 060444
BUCKET					2	BLANK&COMMON
	1	016535	016675		4	BLOCK2
	3	BLOCK1			0	060445 060505
BFLT					2	BLANK&COMMON
	1	016676	017025		4	BLOCK2
	3	BLOCK1			0	060506 060546
HFATFX					2	BLANK&COMMON
	1	017026	017216		4	BLOCK2
	3	BLOCK2			0	060547 060647
PMPONT					2	BLANK&COMMON
	1	017217	017435		4	BLOCK1
	3	BLOCK1			0	060650 060756
PMPREC					2	BLANK&COMMON
	1	017436	017654		4	BLOCK2
	3	BLOCK1			0	060757 061065
BIENDR					2	BLANK&COMMON
	1	017655	017751		4	BLOCK2
	3	BLOCK1			0	061066 061116
CHTFGE					2	BLANK&COMMON
	1	017752	020045		4	BLOCK2
	3	BLOCK1			0	061117 061151
BOWI					2	BLANK&COMMON
	1	020046	020145		4	BLOCK2
	3	BLOCK1			0	061152 061204
SHARP					2	BLANK&COMMON
	1	020146	020245		4	BLOCK2
	3	BLOCK1			0	061205 061237
SCRFFN					2	BLANK&COMMON
	1	020246	020344		4	BLOCK2
	3	BLOCK1			0	061240 061270
GRINDR					2	BLANK&COMMON
	1	020345	020443		4	BLOCK2
	3	BLOCK1			0	061271 061321
RFACTR					2	BLANK&COMMON
	1	020444	020502		4	BLOCK2
					0	061322 061352

Table I.-- Continued.

COLUMN	3	BLOCK1	2	BLANK&COMMON
	1	020543 020725	4	BLOCK2
	3	BLOCK1	0	061553 061416
VFSSEL	1	020726 021142	4	BLANK&COMMON
	3	BLOCK1	0	BLOCK2
	1	021143 021346	4	061417 061503
	3	BLOCK1	0	BLANK&COMMON
STORAG	1	021446 021544	4	BLOCK2
	3	BLOCK1	0	061504 061607
FUPHOR	1	021347 021405	4	BLANK&COMMON
	3	BLOCK1	0	BLOCK2
EVPFRC	1	021446 021544	4	061610 061640
	3	BLOCK1	2	BLANK&COMMON
EVPFLM	1	021545 021637	4	BLOCK2
	3	BLOCK2	0	061641 061671
EVPSPR	1	021640 021734	4	BLANK&COMMON
	3	BLOCK2	0	BLOCK2
BOILER	1	021735 022054	4	061672 061721
	3	BLOCK1	2	BLANK&COMMON
DRYFRR	1	022055 022361	4	BLOCK1
	3	BLOCK2	0	061722 061752
DRYFRP	1	022362 022461	4	BLANK&COMMON
	3	BLOCK1	4	BLOCK2
DRYFR	1	022462 022561	4	061753 062012
	3	BLOCK1	2	BLANK&COMMON
HAMMER	1	022562 022675	4	BLOCK2
	3	BLOCK1	0	062013 062165
SCREW	1	022676 023154	4	BLANK&COMMON
	3	BLOCK1	2	BLOCK2
PULVER	1	023155 023254	4	062166 062220
	3	BLOCK1	4	BLANK&COMMON
CONJFN	1	023255 023345	4	BLOCK2
	3	BLOCK1	0	062221 062253
STLO	1	023346 023467	4	BLANK&COMMON
	3	BLOCK1	2	BLOCK2
HOPPER	1	023470 023567	4	062254 062307
	3	BLOCK1	2	BLANK&COMMON
PRESCK	1	023570 024234	4	BLOCK2
	3	BLOCK1	4	062310 062435
XIPA	1	024235 030602	4	BLANK&COMMON
	3	BLOCK1	2	BLOCK2
	1	02471 062521	4	062436 062470
	3	BLOCK1	2	BLANK&COMMON
	1	062522 062571	4	BLOCK2
	3	BLOCK1	4	062471 062521
	1	062572 062622	4	BLANK&COMMON
	3	BLOCK1	2	BLOCK2
	1	062623 063630	4	062572 062622
	3	BLOCK1	4	BLANK&COMMON
	1	063631 065313	4	BLOCK2
	3	BLOCK1	0	065313

Table I.--Continued.

BIODIG	3	BLOCK1	2	BLANKCOMMON
	5	BLOCK4	4	BLOCK2
	1	032003	0	065314 066246
	3	BLOCK1	2	BLANKCOMMON
PRSTPA	1	035153	0	BLOCK2
	3	BLOCK2	0	066247 067656
	5	BLOCK1	4	BLANKCOMMON
FPCXX1	1	040772	6	DATA1
	3	BLOCK4	0	BLOCK4
	5	BLOCK2	2	067657 070456
MAIN	1	043007	4	BLANKCOMMON
	3	BLOCK1	0	BLOCK1
	5	BLOCK4	2	070457 071006
			2	BLANKCOMMON
			4	BLOCK2

SYS**RLIBS. LEVEL 53.29
 END OF COLLECTION - TIME 4.470 SECONDS

QFIN

RUNID: 7053 ACCOUNT: 154-04-105 PROJECT: FISHFISH

LOAD P0111N 3/0 A -1 7053

SERVICE 3/0 P0111N : 7053

TIME: 00:01:02.380 IN: 54 OUT: 0 PAGES: 137

MEMORY TIME: 0:02:50.430

INITIATION TIME: 11:01:32-000 12.1071

TERMINATION TIME: 11:07:11-000 12.1071

Table II.- IPA plant cost analysis.

IPA PLANT COST ANALYSIS

INPUT DATA

PLANT SIZE = 200.00 TONS/DAY
 MARSHAL/STEVENS INDEX = 1.135
 COST OF FISH = 1.00 CENTS/LB
 ELECTRICITY COSTS = 1.50 CENTS/KWH
 FUEL COST = .06 DOLLARS/THERM
 LABOR AND SUPV. COSTS = 4.00 DOLLARS/HR
 DEPRECIATION AND INT. CHARGE = 15.00 PERCENT

FISH COMPOSITION

OIL = 4.00 PERCENT
 PROTEIN = 16.00
 ASH = 3.00
 WATER = 77.00

OPERATING OPTIONS

OPERATING DAYS PER YEAR = 200.

Table II.-- Continued.

DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOLLARS)

EQUIPMENT TYPE	CAPACITY	MATERIAL	BASE COST	MATERIALS COSTS	LABOR COSTS	INDIRECT COSTS	MODULE COST	RANGE + OR -
FISH PUMPS	1301. GPM TIMES PSI	STEEL	3.919	2.783	2.743	3.488	12.934	1.293
BELT CONVEYER	100.000 FEET(LENGTH)		18.796	5.075	7.330	7.518	38.719	3.872
WATER DUMP TANK	6000. GALLONS	STEEL	2.379	.904	.238	1.165	4.686	.469
MECHANICAL REFRIGERAT.	300.000 TONS		347.856	59.136	48.700	38.264	493.956	49.396
REDWOOD STORAGE BIN	32500. CUBIC FEET	REDWOOD	11.747	2.349	1.175	4.699	19.970	1.175
BRINE MAKE-UP+SALT STOR.			1.190				1.190	
CENTRIFUGAL PUMP	71. GPM TIMES PSI	BRONZE	.512	.364	.140	.225	1.241	.124
CENTRIFUGAL PUMP	65.487 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
BUCKET CONVEYER	20.000 FEET(HEIGHT)	SS	1.750	.487	.984	.700	3.920	.392
PULVERIZER	16666.667 POUNDS/HOUR	SS	17.727	4.822	5.637	7.091	35.277	3.528
SHOP FAB. STORAGE TANK	3500. GALLONS	SST	6.303	2.395	6.303	3.088	18.089	1.809
CENTRIFUGAL PUMP	1000.400 GPM TIMES PSI	SST	1.095	.778	.199	.482	2.554	.255
CENTRIFUGAL PUMP	3123.715 GPM TIMES PSI	SST	1.423	1.010	.258	.626	3.317	.332
AGITATOR-PROPELLAR	17.500 HORSEPOWER	SS	1.662	.459	.572	.665	3.357	.336
SHOP FAB. STORAGE TANK	3200. GALLONS	SST	6.108	2.321	6.108	2.093	17.530	1.753
CENTRIFUGAL PUMP	1698.652 GPM TIMES PSI	SST	1.218	.865	.221	.536	2.839	.284
CENTRIFUGAL PUMP	1698.652 GPM TIMES PSI	SST	1.218	.865	.221	.536	2.839	.284
JACKETED REACTOR VESSEL	6000. GALLONS	SST	18.310	6.958	1.831	8.972	36.071	3.607
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627
AGITATOR-PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
JACKETED REACTOR VESSEL	3200. GALLONS	SST	14.694	5.584	1.469	7.200	28.948	2.895
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627

Table II.--Continued.

AGITATOR=PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
JACKETED REACTOR VESSEL	3200. GALLONS	SST	14.694	5.584	1.469	7.200	28.948	2.895
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.815	6.274	.627
AGITATOR=PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
JACKETED REACTOR VESSEL	3200. GALLONS	SST	14.694	5.584	1.469	7.200	28.948	2.895
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627
AGITATOR=PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	412.565 GPM TIMES PSI	SST	.976	.693	.177	.429	2.275	.227
CENTRIFUGAL PUMP	315.100 GPM TIMES PSI	SST	.956	.679	.173	.421	2.230	.223
CENTRIFUGAL PUMP	297.519 GPM TIMES PSI	SST	.953	.677	.173	.419	2.222	.222
CENTRIFUGAL PUMP	2025.850 GPM TIMES PSI	SST	1.269	.901	.230	.558	2.959	.296
CENTRIFUGAL PUMP	290.051 GPM TIMES PSI	SST	.952	.676	.173	.419	2.219	.222
CENTRIFUGAL PUMP	2008.268 GPM TIMES PSI	SST	1.266	.899	.230	.557	2.952	.295
CENTRIFUGAL PUMP	2000.800 GPM TIMES PSI	SST	1.265	.898	.229	.557	2.950	.295
HEAT EXCHANGER	100.000 SURFACE SQ FT.	ST/ST	2.249	1.606	1.417	2.130	7.403	1.258
DRYER	73.450 AREA(SQ.FEET)	SST	50.846	4.926	3.531	2.825	28.936	2.894
STRIPPER DRYER	73.450 AREA(SQ.FEET)	SST	62.772	5.473	3.923	3.139	32.151	3.215
SCREW CONVEYER	6.000 FEET	SS	.998	.271	.317	.399	1.985	.100
STRIPPER DRYER	73.450 AREA(SQ.FEET)	SST	62.772	5.473	3.923	3.139	32.151	3.215
CONDITIONER	73.450 AREA(SQ.FEET)	SST	62.772	5.473	3.923	3.139	32.151	3.215
SCREW CONVEYER	6.000 FEET	SS	.998	.271	.317	.399	1.985	.100
SCREW CONVEYER	20.000 FEET	SS	2.055	.559	.653	.822	4.089	.205
HAMMER MILL	3.727 TONS PER HR.	SST	1.736	.469	.748	.764	3.717	.372
BAGGING MACHINE	1.725 BAGS/MIN	SS	5.795	2.318	.637	2.318	11.068	1.107

Table II.-- Continued.

ACID STORAGE TANK	38. GALLONS	SST	2.367	.473	.200	1.160	4.199	.420
CENTRIFUGAL PUMP	1,506 GPM TIMES PSI	SST	.772	.548	.140	.340	1.800	.180
CENTRIFUGAL PUMP	2711.150 GPM TIMES PSI	STEEL	.709	.503	.248	.312	1.772	.177
SHOP FAB. STORAGE TANK	1301. GALLONS	STEEL	1.393	.529	4.458	.683	7.063	.706
CENTRIFUGAL PUMP	2711.150 GPM TIMES PSI	STEEL	.709	.503	.248	.312	1.772	.177
DISK TYPE CENTRIFUGE	20,000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
DISK TYPE CENTRIFUGE	20,000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
DISK TYPE CENTRIFUGE	20,000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
CENTRIFUGAL PUMP	43,746 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
SHARPLES CENTRIFUGE	20,000 HORSEPOWER	SS	45.257	11.767	15.387	18.103	90.514	9.051
SHOP FAB. STORAGE TANK	3077. GALLONS	SST	13.489	5.126	13.489	6.610	38.714	3.871
CENTRIFUGAL PUMP	.427 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
SHOP FAB. STORAGE TANK	5383. GALLONS	SST	7.327	2.784	7.327	3.590	21.030	2.103
CENTRIFUGAL PUMP	26,913 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
CENTRIFUGAL PUMP	26,913 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
HEAT EXCHANGER	448,365 SURFACE SQ FT. ST/ST		5.720	4.084	3.603	5.417	18.824	3.200
CENTRIFUGAL PUMP	780,882 GPM TIMES PSI	STEEL	.545	.387	.191	.240	1.363	.136
DISK TYPE CENTRIFUGE	20,000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
HEAT EXCHANGER	4283,600 SURFACE SQ FT. ST/ST		23.283	16.624	14.669	22.049	76.626	13.026
SHOP FAB. STORAGE TANK	4002. GALLONS	SST	6.605	2.510	6.605	3.237	18.957	1.896
CENTRIFUGAL PUMP	1980,792 GPM TIMES PSI	STEEL	.654	.464	.229	.288	1.635	.163
DIST. COLUMN SHELL	1526,813 CUBIC FEET	SS	65.250	18.455	17.637	21.335	122.677	6.525
DISTILLATION COLUMN	54,000 FEET(HIGHT)	SS	10.605	2.273	3.030	3.030	18.938	1.061
SHOP FAB. STORAGE TANK	14406. GALLONS	STEEL	3.232	1.228	10.342	1.584	16.385	1.639
CENTRIFUGAL PUMP	.200 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
HEAT EXCHANGER	13374,648 SURFACE SQ FT. ST/ST		47.272	33.753	29.782	44.767	155.574	26.448
CENTRIFUGAL PUMP	200,000 GPM TIMES PSI	STEEL	.487	.346	.170	.214	1.217	.122
SHOP FAB. STORAGE TANK	1577. GALLONS	SST	4.768	1.812	4.768	2.336	13.684	1.368
CENTRIFUGAL PUMP	7,884 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100

Table II.--Continued.

VERTICAL EVAPORATOR	662.220	SURFACE SQ FT, SST	10.221	6,746	2.453	4.293	23.713	2.371
VERTICAL EVAPORATOR	662.220	SURFACE SQ FT, SST	10.221	6,746	2.453	4.293	23.713	2.371
VERTICAL EVAPORATOR	662.220	SURFACE SQ FT, SST	10.221	6,746	2.453	4.293	23.713	2.371
VERTICAL EVAPORATOR	79.588	SURFACE SQ FT, SST	3.325	2,195	.798	1.397	7.715	.771
CENTRIFUGAL PUMP	59.691	GPM TIMES PSI STEEL	.400	.284	.140	.176	1.000	.100
SHOP FAB. STORAGE TANK	29.	GALLONS STEEL	.678	.136	.183	.332	1.329	.133
CENTRIFUGAL PUMP	.597	GPM TIMES PSI STEEL	.400	.284	.140	.176	1.000	.100
SHOP FAB. STORAGE TANK	42977.	GALLONS STEEL	4.738	1,800	15.161	2.322	24.021	2.402
BOILER	62097.921	POUNDS/HOUR SS	124.585	23,671	18.688	24,917	191.861	19,186
SHOP FAB. STORAGE TANK	19169.	GALLONS STEEL	3.572	1,357	11.429	1.750	18.108	1.811
CENTRIFUGAL PUMP	.266	GPM TIMES PSI STEEL	.400	.284	.140	.176	1.000	.100
CONTROL INSTRUMENTATION			87.000				1.000	
PAYLOADER			20.000				20.000	
SCRUBBERS	200.000	TONS PROCESSED STEEL	4.540	1,498	1.498	1.498	9.034	.454
BOILER WATER TREATMENT			1.000				1.000	
SEA WATER PUMPS	8179.034	GPM TIMES PSI BRONZE	1.300	.923	.355	.572	3.151	.315
CARBON ADSORBER			2.000				2.000	
VENT CONDENSER	20.000	SURFACE SQ FT, ST/SST	1.860	1,328	.521	1.761	5.470	.930
SCALE	18.000	TONS SS	4.540	.363	.000	1.816	6.719	.454
SCALE	18.000	TONS SS	4.540	.363	.000	1.816	6.719	.454
SCALE	18.000	TONS SS	4.540	.363	.000	1.816	6.719	.454
SCALE	18.000	TONS SS	4.540	.363	.000	1.816	6.719	.454
TOTAL COSTS			1400.533	331,836	319,878	359,491	2163,078	221,047

Table II.-- Continued.

MATERIAL AND ENERGY INFORMATION

GENERAL

FISH = 200,000 TONS/DAY
 OF WHICH 4.00 PERCENT OR 8,000 - IS OIL
 16.00 - OR 32,000 - PROTEIN
 3.00 - OR 6,000 - ASH

PROCESS STEAM = 62098. LB/HR
 PROCESS COOLING WATER = 408952. GAL/HR
 ELECTRICITY 12214. KWHR

EQUIPMENT FLOW RATES

FISH TO EXTRACTION VESSELS 16667. LB/HR

STEAM(STIRRED VESSEL 1) 140. LB/HR
 STEAM(STIRRED VESSEL 2) 80. LB/HR
 STEAM(STIRRED VESSEL 3) 80. LB/HR
 STEAM(STIRRED VESSEL 4) 80. LB/HR
 STEAM(PREHEATER-DISTILLATION) 4484. LB/HR
 STEAM(REBOILER) 42836. LB/HR
 STEAM(ROTARY DRYER FPC) 2348. LB/HR
 STEAM(ROTARY DRYER BONE MEAL) 0. LB/HR
 COOLING WATER CONDENSER 24892. GAL/HR
 COOLING WATER DISTILLATION COND. 2676. GAL/MIN
 TOTAL STEAM 62098. LB/HR
 TOTAL WATER 3406568. LB/HR

	STREAM 1	STREAM 2	STREAM 3	STREAM 4	STREAM 5
RAFFINATE OIL	7.951	1.311	.345	.148	.000
RAFFINATE ASH	1.532	.192	.095	.047	.000
RAFFINATE PROTEIN	7.163	.763	.251	.251	.000

Table II.-- Continued.

RAFFINATE WATER	152.199	42.859	23.209	13.205	.000
RAFFINATE ALCOHOL	373.968	379.368	381.108	387.842	400.000
EXTRACT OIL	8.000	1.360	.394	.197	.049
EXTRACT ASH	6.000	4.860	4.763	4.715	4.668
EXTRACT PROTEIN	32.000	25.600	25.088	25.088	24.837
EXTRACT WATER	154.000	44.660	25.010	15.006	1.801
EXTRACT ALCOHOL	.000	6.000	7.740	14.474	26.632
FLOW FROM EXTRACTION VESSEL 4	4832. LB/HR				
FLOW FROM EXTRACTION VESSEL 1	45168. LB/HR				
AQUEOUS STREAM(CENTRIFUGE)	44882. LB/HR				
TOPS FROM DISTILLATION COLUMN	31088. LB/HR				
BOTTOMS FROM DISTILLATION COLUMN	13009. LB/HR				
OIL FROM SECOND CENTRIFUGE	331. LB/HR				
FISH OIL PRODUCT	663. LB/HR				
BONE MEAL CONCENTRATE	0. LB/HR				
FISH PROTEIN CONCENTRATE	2588. LB/HR				
FISH SOLUABLES	218. LB/HR				

Table II.--Continued.

COST OF FACILITIES AND SITE DEVELOPMENT							
	UNIT COST	NUMBER OF UNITS	BASE COST	LABOR COSTS	INDIRECT COSTS	TOTAL COSTS	RANGE + OR -
LAND	10.000 PER ACRE	1.000	10.000	.000	.000	10.000	1.500
FENCING	2.673 PER 1000 FT	.833	1.342	.429	.456	2.227	.334
PAVING	1.125 PER 1000 SQ.FT	14.505	5.280	9.240	1.795	16.315	2.447
DOCK FACILITIES	2.496 PER 1000 SQ.FT	2.400	1.560	3.900	.530	5.990	.899
BULK STORAGE WAREHOUSE							
ELECTRICAL WIRING	.900 PER 1000SQ.FT						
FIRE PREVENTION EQP.	1.100 PER 1000SQ.FT						
TOTAL WAREHOUSE	8.770 PER 1000 SQ.FT	.600	3.132	1.065	1.065	5.262	.789
PROCESS BUILDING							
ELECTRICAL WIRING	1.750 PER 1000 SQ.FT						
HEATING AND VENTIL.	1.500 PER 1000 SQ.FT						
PLUMBING(GENERAL)	1.700 PER 1000 SQ.FT						
FIRE PREVENTION EQUIP	1.100PER 1000 SQ.FT						
TOTAL BUILDING COSTS	14.784 PER 1000 SQ.FT	2.600	22.680	7.779	7.779	38.438	5.766
LABORATORY CONTROL INSTRUMENTATION			150.000			150.000	
TOTAL FACILITIES			67.074	30.193	19.405	228.233	17.501

Table II.--Continued.

SUMMARY OF FIXED COSTS

EQUIPMENT	2163.078
SPARE PARTS	28.011
FACILITIES	228.233
ENGINEERING	181.449
CONTINGENCIES	260.077
TOTAL CAPITOL COSTS	2860.848

Table II.-- Continued.

OPERATING COSTS		
COST ITEM	QUANTITY USED	COST IN DOLLARS PER DAY
FISH	200. TONS	4000.00
FUEL OIL	10645. GALLONS	638.72
ELECTRICITY	12214. KWHR	158.78
ANTIOXIDANT	45.38 LB	181.54
PACKAGING	2485. BAGS	621.16
CITY WATER	9814840. GALLONS	2453.71
LABOR AND SUPERVISION	176. MAN HR.	704.00
DEPRECIATION		1430.42
MAINTENANCE		95.36
PAYROLL EXTRAS BOILER WATER TREATMENT		105.60 3.30
INSURANCE AND TAXES		95.36
OVERHEAD		211.20
ISOPROPYL ALCOHOL	8000. POUNDS	516.88
PHOSPHORIC ACID	1084. POUNDS	24.39
TOTAL OPERATING COSTS		11,240.43
PRODUCTION RATE		
BONE MEAL	.000 TONS/DAY	
FISH SOL.	14.326 TONS/DAY	
DRY CONC.	31.058 TONS/DAY	
FISH OIL	7.951 TONS/DAY	
BONE MEAL	0. TONS/YEAR	
FISH SOL.	2865. TONS/YEAR	
DRY CONC.	6212. TONS/YEAR	
FISH OIL	1590. TONS/YEAR	
YEARLY OPERATING COST = .267080+07 DOLLARS		

Table II.-- Continued.

BY-PRODUCT	PRODUCTION COST OF FPC PRICE (CENTS/POUND)	TOTAL WORTH (DOLLARS/YEAR)
FISH OIL	4.0	.127211+06
FISH SOLUBLES	3.5	.200561+06
	FPC COST WITHOUT BY-PRODUCTS	21.5 CENTS/POUND
	FPC COST WITH BY-PRODUCTS	18.9 CENTS/POUND

Table III
 Cost Data for 50 ton/day Capacity Plants

Plant Type	Fish Type	Capital Costs \$·10 ⁶	Yearly Production Rates and Costs					FPC Cost Disregarding by product ¢/lb	FPC with product by ¢/lb
			Bone Meal tons/yr	Fish Paste tons/yr	Dry Con. tons/yr	Fish Oil tons/yr	Operating costs \$·10 ⁶		
Biolog-ical	Fat	1.35	1340	-	1360	900	0.985	36.1	30.
Press Cake-Biolog-ical	Fat	1.41	340	-	1960	950	0.896	22.8	20.3
IPA	Lean	1.58	-	720	1550	400	0.987	31.8	29.1
Press Cake-	Fat	1.57	-	1110	1400	1410	0.879	31.2	25.1
IPA	Lean	1.57	-	1110	1400	400	0.88	31.3	27.4

Table IV
 Cost Data for 200 ton/day Capacity Plants

Plant Type	Fish Type	Capital Costs \$·10 ⁶	Yearly Production Rates and Costs					FPC Cost Disregarding by product ¢/lb	FPC with product by product ¢/lb
			Bone Meal tons/yr	Fish Paste tons/yr	Dry Con. tons/yr	Fish Oil tons/yr	Operating costs \$·10 ⁶		
Biolog-ical	Fat	2.40	5350	-	5450	3600	2.76	25.3	19.2
Press Cake Biolog-ical	Fat	2.65	1380	-	7860	3800	2.40	15.3	12.7
IPA	Lean	2.73	-	2860	6210	1590	2.64	21.2	18.6
Press Cake	Fat	2.82	-	4430	5620	4790	2.22	19.8	13.6
IPA	Lean	2.82	-	4430	5620	1600	2.23	19.8	16.0

Table V
 Cost Data for 1000 ton/day Capacity Plants

Plant Type	Fish Type	Capital Costs \$·10 ⁶	Yearly Production Rates and Costs					FPC Cost Disregarding by product ¢/lb	FPC with product by ¢/lb
			Bone Meal tons/yr	Fish Paste tons/yr	Dry Con. tons/yr	Fish Oil tons/yr	Operating costs \$·10 ⁶		
Biolog-ical	Fat	7.71	26700	-	27300	1800	11.65	21.4	15.3
Press Cake Biolog-ical	Fat	8.01	6900	-	39300	1900	9.70	12.3	9.8
IPA	Lean	7.13	-	14300	31000	7900	10.6	17.1	14.4
Press Cake	Fat	7.023	-	22100	28100	24000	8.41	15.0	8.8
IPA	Lean	7.024	-	22100	28100	8000	8.46	15.0	11.1

Table VI
 Cost Data for Fish Meal Plants

Plant Capacity tons/day	Fish Type	Capital Costs \$·10 ⁶	Yearly Production and Costs		
			Fish Meal tons/yr	Fish Oil tons/yr	Operating costs \$·10 ⁶
50	Fat	.728	2090	1010	0.687
	Lean	.725	1960	340	0.675
200	Fat	1.12	8400	4030	1.72
	Lean	1.11	7860	1340	1.68
1000	Fat	2.84	41800	20000	6.64
	Lean	2.62	39000	6700	6.36



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