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MEMORANDUM

THEORETICAL PERFORMANCE OF LIQUID HYDROGEN WITH
LIQUID OXYGEN AS A ROCKET PROPELLANT

By Sanford Gordon and Bonnie J. McBride

Lewis Research Center
Cleveland, Ohio

NATIONAL AERONAUTICS AND
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Tables II(a) through II(h): Add 10,000 to the enthalpy values for $R = 0.150$ and 0.200 for pressure ratios of 1.00 to 4000.00.

Tables II(a), (c), (d), (e), (g), and (h): Add 10,000 to the enthalpy values for $R = 0.250$ for pressure ratios of 1.00 to 10.00.

Tables II(b) and (f): Add 10,000 to the enthalpy values for $R = 0.250$ for pressure ratios of 1.00 to 10.21.

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THEORETICAL PERFORMANCE OF LIQUID HYDROGEN WITH
LIQUID OXYGEN AS A ROCKET PROPELLANT

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SUMMARY

Theoretical rocket performance for both equilibrium and frozen composition during expansion was calculated for the propellant combination liquid hydrogen and liquid oxygen at four chamber pressures (60, 150, 300, and 600 lb/sq in. abs) and a wide range of pressure ratios (1 to 4000) and oxidant-fuel ratios (1.190 to 39.683). Data are given to estimate performance parameters at chamber pressures other than those for which data are tabulated. The parameters included are specific impulse, specific impulse in vacuum, combustion-chamber temperature, nozzle-exit temperature, molecular weight, molecular-weight derivatives, characteristic velocity, coefficient of thrust, ratio of nozzle-exit area to throat area, specific heat at constant pressure, isentropic exponent, viscosity, thermal conductivity, Mach number, and equilibrium gas compositions.

The maximum value of specific impulse for expansion to 1 atmosphere is given in the following table:

Combustion-chamber pressure, P_c , lb/sq in. abs	Ratio of chamber pressure to exit pressure, P_c/P	Specific impulse, I, (lb)(sec)/(lb)	
		Assuming frozen composition	Assuming equilibrium composition
60	4.083	254.6	255.4
150	10.207	313.1	315.0
300	20.414	345.8	348.1
600	40.827	371.8	374.5

INTRODUCTION

The performance of hydrogen and oxygen as a rocket propellant has been reported in the literature. However, additional performance calculations are needed for a wider range of conditions than were heretofore available. Calculations were therefore made at the NASA Lewis Research Center to provide rocket performance data for liquid hydrogen and liquid oxygen for the following conditions:

- (1) Four chamber pressures (60, 150, 300, and 600 lb/sq in. abs)
- (2) A wide range of oxidant-fuel weight ratios (1.190 to 39.683)
- (3) A wide range of pressure ratios (1 to 4000)
- (4) Equilibrium and frozen composition during expansion

Data are given to permit estimates of performance parameters at chamber pressures other than those given in this report.

SYMBOLS

The following symbols are used in this report:

A	nozzle area, sq in.
\mathcal{A}	number of formula weights (defined as A in ref. 1)
a	local velocity of sound, ft/sec
C_F	coefficient of thrust, $C_F = g_c I / c^* = F / P_c A_t$
C_p^0	molar specific heat at constant pressure, cal/(mole)(°K)
c_p	specific heat at constant pressure, $(\partial h / \partial T)_P$, cal/(g)(°K)
c_v	specific heat at constant volume, cal/(g)(°K)
c^*	characteristic velocity, $g_c P_c A_t / w$, ft/sec
F	thrust, lb
$f_{\mu}^{(k)}$	function of T^*
g_c	gravitational conversion factor, $32.174 \left(\frac{\text{lb mass}}{\text{lb force}} \right) \left(\frac{\text{ft}}{\text{sec}^2} \right)$

H_T^O	sum of sensible enthalpy and chemical energy at temperature T, cal/mole
h	sum of sensible enthalpy and chemical energy per unit mass, $\frac{\sum_i x_i (H_T^O)_i}{M}, \text{ cal/g}$
I	specific impulse with ambient and exit pressures equal, (lb force)(sec)/lb mass
I_{vac}	specific impulse in vacuum, (lb force)(sec)/lb mass
k	coefficient of thermal conductivity, cal/(sec)(cm)(°K)
M	Mach number
M	molecular weight, $\sum_i x_i M_i$, g/g-mole or lb/lb-mole
n_{c^*}	characteristic-velocity exponent, $\partial \ln c^* / \partial \ln P_c$
n_I	specific-impulse exponent for fixed pressure ratio, $\left(\frac{\partial \ln I}{\partial \ln P_c} \right)_{P_c/P}$
$n_{I_{vac}}$	specific-impulse in vacuum exponent for fixed pressure ratio, $\left(\frac{\partial \ln I_{vac}}{\partial \ln P_c} \right)_{P_c/P}$
n_T	temperature exponent for fixed pressure ratio, $\left(\frac{\partial \ln T}{\partial \ln P_c} \right)_{P_c/P}$
n_ϵ	area-ratio exponent for fixed pressure ratio, $\left(\frac{\partial \ln \epsilon}{\partial \ln P_c} \right)_{P_c/P}$
O/F	oxidant-fuel weight ratio
P	static pressure (sum of partial pressures), lb/sq in. abs
p	partial pressure, lb/sq in. abs
Q	heat of formation or dissociation

R	equivalence ratio, ratio of two times the number of oxygen atoms to the number of hydrogen atoms, $2(O)/(H)$
\mathcal{R}	universal gas constant (consistent units)
S_T^0	entropy at a pressure of 1 atmosphere, $\text{cal}/(\text{mole})(^\circ\text{K})$
s	entropy per unit mass, $\frac{\sum_i x_i [(S_T^0)_i - \mathcal{R} \ln(p_i/14.696)]}{\mu}$, $\text{cal}/(\text{g})(^\circ\text{K})$
T	temperature $^\circ\text{K}$
T^*	reduced temperature for viscosity calculations (temperature divided by force constant (ϵ/k)), kT/ϵ
V	velocity, ft/sec
v	specific volume
w	mass-flow rate, lb/sec
x	mole fraction
γ	isentropic exponent, $\left(\frac{\partial \ln P}{\partial \ln \rho}\right)_s$
δ	correction term for polarity for viscosity calculations
ϵ	ratio of nozzle area to throat area
ϵ/k	force constant for viscosity calculation
μ	absolute viscosity, $\text{g}/(\text{cm})(\text{sec})$ or poises
ρ	density, $\text{lb}/\text{cu in.}$
σ	collision diameter for viscosity calculation
$\Omega(2,2)^*$	function of T^*

Subscripts:

c	combustion chamber
e	nozzle exit

i	product of combustion
in	injector
P	constant pressure
P_c/P	constant pressure ratio
s	constant entropy
T	constant temperature
t	nozzle throat
l	reference point

Superscript:

o	thermodynamic standard reference state
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CALCULATION OF PERFORMANCE DATA

Theoretical rocket performance data were obtained for liquid hydrogen with liquid oxygen for four chamber pressures over a wide range of oxidant-fuel ratios and pressure ratios assuming both equilibrium and frozen composition during expansion.

The computations were carried out by the method of reference 1 with modifications to adapt it for use with an IBM 650 Magnetic Drum Data-Processing Machine, with index accumulators, high-speed core, and floating-point attachments. The successive approximation process used in the calculations was continued until seven-figure accuracy was reached in the desired values of the assigned parameters (mass balance, pressure, and enthalpy or entropy).

Assumptions

The calculations were based on the following usual assumptions: perfect gas law, adiabatic combustion at constant pressure, isentropic expansion, no friction, homogeneous mixing, and one-dimensional flow. The products of combustion were assumed to be the following ideal gases: atomic hydrogen, H; hydrogen, H_2 ; water, H_2O ; atomic oxygen, O; oxygen, O_2 ; and the hydroxyl radical, OH.

Initial Data

Thermodynamic data. - The ideal gas thermodynamic properties for atomic hydrogen, hydrogen, atomic oxygen, and oxygen were taken from reference 2. Data for water are also given in reference 2, however, the same data are given to more decimal places in reference 3, and therefore reference 3 data were used. The hydroxyl radical data were taken from reference 4. The values of entropy used in the present report do not include nuclear spin.

Heats of formation or dissociation. - The heats of formation or dissociation for the molecules considered in this report are given in the following table:

Reaction (all substances in gas phase)	Heat of formation or dissociation, Q		Temperature of reaction, $^{\circ}\text{K}$	Reference
	cm^{-1}	cal/mole		
$\text{Q} + \text{H}_2 \rightarrow 2\text{H}$	36,116	103,263	0	5
$\text{Q} + \text{O}_2 \rightarrow 2\text{O}$	41,260	117,971	0	6
$\text{H}_2 + \frac{1}{2} \text{O}_2 \rightarrow \text{H}_2\text{O} + \text{Q}$	-----	57,797.9	298.16	7
$\text{Q} + \text{OH} \rightarrow \text{O} + \text{H}$	35,450	101,389	0	8

Where values are given in centimeter^{-1} , they are converted by taking 1 centimeter^{-1} equivalent to 2.85921 calories per mole, calculated from data given in reference 9. The base used in this report for assigning absolute values to enthalpy is the same as in reference 1.

Viscosity data. - Viscosity data are needed for heat-transfer calculations; however, accurate data for gases at high temperatures are unavailable in the literature. Theoretical considerations of force fields lead to theoretical expressions for viscosity that fit available experimental data fairly well and therefore provide a basis upon which experimental data may be extrapolated into the higher temperature regions.

A detailed treatment of the derivation of various theoretical equations for viscosity is given in references 10 and 11. The use of these equations to obtain a refined numerical calculation of viscosity involves the selection of a force-field potential and considerable numerical work. Much of this numerical work can be saved by using tables of collision integrals such as those based on the Lennard-Jones 6-12 potential and the following equation (ref. 11):

$$\mu \times 10^7 = \frac{266.93 \sqrt{T} f_{\mu}^{(k)}}{\sigma^2 \Omega(2,2)^*} \quad (1)$$

The parameters $\Omega(2,2)^*$ and $f_{\mu}^{(k)}$ for nonpolar gases are tabulated in reference 11 as a function of reduced temperature T^* while $\Omega(2,2)^*$ for polar gases ($f_{\mu}^{(k)}$ assumed to be unity) is tabulated in reference 12 as a function of T^* and δ .

The force constants ϵ/k and σ for H_2 , O_2 , and H and ϵ/k , σ , and δ for H_2O were calculated from experimental viscosity data. No experimental viscosity data were found for O and OH. The value of σ for O was estimated from equations in reference 13, and the value of ϵ/k was taken to be equal to that of O_2 . The values of σ and ϵ/k for OH were estimated from the following equations:

$$\sigma_{OH} = \frac{\sigma_{O_2} + \sigma_{H_2}}{2} \quad (2)$$

$$(\epsilon/k)_{OH} = \sqrt{(\epsilon/k)_{O_2} (\epsilon/k)_{H_2}} \quad (3)$$

The force constants selected are summarized in the following table:

Sub-stance	σ , Å	ϵ/k , °K	δ	Refer-ence
H	2.497	99.8		a ₁₄
H ₂	2.729	86.1		a ₂
H ₂ O	3.487	126.3	2.409	a ₁₅
O	3.068	102.2		b ₁₃
O ₂	3.490	102.2		a ₂
OH	3.110	93.8		(c)

^aCalculated from data in reference given.

^b σ Estimated from equations in reference given and ϵ/k assumed equal to that of O_2 .

^cEstimated by means of equations (2) and (3).

Physical and thermochemical data. - Several physical and thermochemical properties of the propellants are listed in table I. Additional properties of hydrogen may be found in references 16 and 17 while properties of oxygen may be found in reference 18.

FORMULAS

The formulas used in computing the various performance parameters are as follows:

Specific impulse with ambient and exit pressures equal, (lb force)(sec)/lb mass:

$$I = 294.98 \sqrt{\frac{h_c - h_e}{1000}} \quad (4)$$

Specific impulse in vacuum, (lb force)(sec)/lb mass:

$$I_{vac} = I + P \left(\frac{A}{w} \right) \quad (5)$$

Nozzle area per unit mass-flow rate, (sq in.)(sec)/lb:

$$\frac{A}{w} = \frac{86.4554 T}{P_c I} \quad (6)$$

Throat area per unit mass-flow rate, (sq in.)(sec)/lb:

$$\frac{A_t}{w} = \frac{2781.6 T_t}{P_t A_t} \quad (7)$$

This equation is derived from the continuity equation and the fact that velocity of flow equals velocity of sound at the throat.

Velocity of sound, ft/sec:

$$a = \sqrt{\left(\frac{\partial P}{\partial \rho} \right)_s} = \sqrt{\frac{P}{\rho} \left(\frac{\partial \ln P}{\partial \ln \rho} \right)_s} = 299.16 \sqrt{\left(\frac{T}{\mu} \right) \left(\frac{\partial \ln P}{\partial \ln \rho} \right)_s} \quad (8)$$

Characteristic velocity, ft/sec:

$$c^* = g_c P_c \frac{A_t}{w} = 32.174 P_c \frac{A_t}{w} \quad (9)$$

Coefficient of thrust:

$$C_F = \frac{g c^* I}{c^*} = \frac{32.174 I}{c^*} \quad (10)$$

Ratio of nozzle area to throat area

$$\epsilon = \frac{A/w}{A_t/w} \quad (11)$$

Partial Derivatives .

The derivatives of the fundamental thermodynamic quantities have many useful applications. Equations (24) to (27) are examples of these applications.

All the relations between first derivatives may be expressed in terms of three arbitrary first derivatives in addition to the fundamental quantities. The three derivatives selected for this report are $(\partial h/\partial T)_P = c_p$, $(\partial \ln \mathcal{M}/\partial \ln T)_P$, and $(\partial \ln \mathcal{M}/\partial \ln P)_T$. Specific heat c_p is needed in heat-transfer calculations and the other two derivatives are a useful indication of the extent of dissociation.

These derivatives were obtained by means of the following equations:

$$c_p = \frac{1}{P \mathcal{M} T} \left[\sum_i P_i (H_T^0)_i \left(\frac{\partial \ln p_i}{\partial \ln T} \right)_P - \mathcal{M} h \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P + T \sum_i P_i (C_P^0)_i \right] \quad (12)$$

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \frac{P}{\sum_i P_i \left(\frac{\partial \ln p_i}{\partial \ln \mathcal{M}} \right)_T} - 1 \quad (13)$$

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P = \left(\frac{\partial \ln \mathcal{A}}{\partial \ln T} \right)_P \quad (14)$$

where $(\partial \ln p_i/\partial \ln T)_P$, $(\partial \ln \mathcal{A}/\partial \ln T)_P$, and $(\partial \ln p_i/\partial \ln \mathcal{A})_T$ are found by matrix methods similar to those described for obtaining $(\partial \ln p_i/\partial \ln T)_S$ in reference 1, and where \mathcal{A} is A in reference 1.

Reference 19 presents a convenient scheme for expressing all first derivatives in terms of $(\partial v/\partial T)_P$, $(\partial v/\partial P)_T$, and $(\partial h/\partial T)_P = c_p$. By means

of the following equations, $(\partial v/\partial T)_P$ and $(\partial v/\partial P)_T$ can be obtained from the derivatives given in this report:

$$\left(\frac{\partial v}{\partial T}\right)_P = -\frac{v}{T} \left[\left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P - 1 \right] \quad (15)$$

$$\left(\frac{\partial v}{\partial P}\right)_T = -\frac{v}{P} \left[\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T + 1 \right] \quad (16)$$

With the aid of the tables in reference 19 and equations (15) and (16), other first derivatives can be expressed in terms of c_p , $(\partial \ln \mathcal{M}/\partial \ln T)_P$, and $(\partial \ln \mathcal{M}/\partial \ln P)_T$. Some examples are,

$$c_v = c_p - \frac{\mathcal{R}}{\mathcal{M}} \frac{\left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P \right]^2}{1 + \left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T} \quad (17)$$

$$\gamma = \left(\frac{\partial \ln P}{\partial \ln \rho}\right)_s = \frac{c_p}{c_p \left[1 + \left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T \right] - \frac{\mathcal{R}}{\mathcal{M}} \left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P \right]^2} \quad (18)$$

or

$$\gamma = \frac{c_p}{c_v} \left[\frac{1}{1 + \left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T} \right] \quad (19)$$

When composition is frozen,

$$\left(\frac{\partial \ln \mathcal{M}}{\partial \ln P}\right)_T = \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P = 0 \quad (20)$$

and equations (17) and (18) reduce to

$$c_v = c_p - \frac{\mathcal{R}}{\mathcal{M}}$$

and

$$\gamma = \frac{c_p}{c_p - \frac{\mathcal{R}}{\mathcal{M}}} = \frac{c_p}{c_v} \quad (21)$$

Viscosity of Mixtures

Viscosities of multicomponent mixtures calculated by rigorous methods (refs. 11 and 20) show excellent agreement with experimental data. However, these calculations involve considerable effort and become increasingly more difficult with increasing number of components. Simpler techniques, but which still involve considerable calculations, are given in references 21 and 22.

The following equation, based on averaging kinematic viscosities, gives approximate results, which are often sufficiently accurate for engineering purposes:

$$\mu = \frac{\mathcal{M}}{\sum_1 \frac{x_1 \mathcal{M}_1}{\mu_1}} \quad (22)$$

The equation appears adequate until better high-temperature data for the individual components become available.

Conductivity

Thermal conductivities as well as viscosities are needed in heat-transfer calculations. However, experimental conductivity data are generally even less available than experimental viscosity data. Therefore, the Eucken relation

$$k = \mu \left(c_p + \frac{5}{4} \frac{\mathcal{R}}{\mathcal{M}} \right) \quad (23)$$

which often gives satisfactory values of conductivity for individual components, is used in this report to estimate the conductivity of gaseous mixtures.

THEORETICAL PERFORMANCE DATA

Tables

The calculated values of the various performance parameters for combustion pressures of 60, 150, 300, and 600 pounds per square inch absolute and for a range of equivalence ratios and exit conditions are given in tables II to V. Table II presents performance data at assigned pressure ratios from 1 to 4000 for equivalence ratios from 0.15 to 5.00 (oxidant-fuel weight ratios from 1.190 to 39.683). Properties at the throat may be found where $\epsilon = 1.00$. Table III gives various thermodynamic partial

derivatives. Equilibrium composition in the combustion chamber and at the assigned exit conditions is given in table IV. Characteristic velocity and summary of the performance parameters at an exit pressure of 1 atmosphere are presented in table V.

Curves

The performance parameters are plotted in figures 1 to 8. Curves of specific impulse are presented in figure 1 for assigned pressure ratios as functions of percent by weight of fuel. Combustion temperature and exit temperature for assigned pressure ratios are plotted in figure 2 as functions of percent by weight of fuel. Curves of the ratio of nozzle area to throat area are plotted in figure 3 as functions of percent by weight of fuel for assigned pressure ratios. Figure 4 gives the curves for coefficient of thrust for assigned pressure ratios as functions of percent by weight of fuel; figure 5 presents curves of molecular weight for assigned pressure ratios; and figure 6 presents curves of characteristic velocity as functions of percent by weight of fuel. Figure 7 gives curves of specific impulse in vacuum for assigned area ratios as functions of percent by weight of fuel. The curves of figure 7 were obtained by interpolation of the data at assigned pressure ratios.

Effect of Assuming Frozen or Equilibrium Composition During Expansion

A comparison of specific impulse data based on equilibrium and frozen composition during expansion to an exit pressure of 1 atmosphere is given in figure 8. A comparison of maximum calculated values of specific impulse based on equilibrium and frozen composition during expansion is shown in the following table for expansion to 1 atmosphere and to pressure ratios of 100 and 4000 (taken from table II):

Chamber pressure, P_c , lb/sq in. abs	Pressure ratio, P_c/P	Equivalence ratio, R, at which I is maximum	Oxidant-fuel weight ratio, O/F	Composition during expansion	Maximum specific impulse, I, (lb)(sec)/lb	Difference in I, percent
60	4.083	0.35	2.778	Equilibrium	255.4	0.31
		.35	2.778	Frozen	254.6	
	100	0.45	3.571	Equilibrium	400.8	1.67
		.40	3.175	Frozen	394.2	
60	4000	0.70	5.556	Equilibrium	465.9	3.81
		.40	3.175	Frozen	448.8	
150	10.207	0.40	3.175	Equilibrium	315.0	0.61
		.35	2.778	Frozen	313.1	
	100	0.50	3.968	Equilibrium	401.3	1.42
		.40	3.175	Frozen	395.7	
150	4000	0.70	5.556	Equilibrium	466.6	3.37
		.45	3.571	Frozen	451.4	
300	20.414	0.45	3.571	Equilibrium	348.1	0.67
		.40	3.175	Frozen	345.8	
	100	0.50	3.968	Equilibrium	401.5	1.24
		.40	3.175	Frozen	396.6	
300	4000	0.70	5.556	Equilibrium	467.0	3.02
		.45	3.571	Frozen	453.3	
600	40.827	0.50	3.968	Equilibrium	374.5	0.73
		.40	3.175	Frozen	371.8	
	100	0.50	3.968	Equilibrium	401.7	1.06
		.45	3.571	Frozen	397.5	
600	4000	0.70	5.556	Equilibrium	467.4	2.75
		.50	3.968	Frozen	454.9	

The preceding table shows that for pressure ratios up to 100, the difference in maximum specific impulse due to equilibrium or frozen composition during expansion is less than 2 percent. For a pressure ratio of 4000 the difference increases to 3 to 4 percent. However, the maximum specific impulse occurs in general at a higher oxidant-fuel ratio O/F for equilibrium composition than for frozen composition.

A comparison of values of maximum specific impulse for frozen and equilibrium composition at the same O/F ratio could show larger differences. For example, from data in table II, for a chamber pressure of 60 pounds per square inch

absolute, a pressure ratio of 4000, an O/F of 5.556 (where equilibrium specific impulse is maximum) the difference in specific impulse for frozen and equilibrium composition is 9.6 percent. For the same conditions but for the stoichiometric O/F of 7.937, the difference is 15.8 percent. This is the largest difference between frozen and equilibrium specific impulse at constant O/F for any of the conditions in this report.

The O/F for maximum specific impulse increases with increasing pressure ratio. For fixed pressure ratios and frozen composition the O/F for maximum specific impulse increases with increasing chamber pressure.

Effect of Chamber Pressure

By use of suitable exponents, performance parameters can be estimated with good accuracy at chamber pressures other than those given in this report. The logarithmic values of the parameters I , I_{vac} , T , ϵ , and c^* are very nearly linear with the logarithm of chamber pressure for a fixed equivalence ratio and pressure ratio or fixed equivalence ratio and area ratio. This linearity permits the data to be extended by means of exponential equations.

In the case of equilibrium composition, the following analytic expressions were derived that permit the exponents to be computed from data at a single chamber pressure:

$$n_I = \left(\frac{\partial \ln I}{\partial \ln P_c} \right)_{P_c/P} = 86.4554 \frac{T}{I^2} \left(\frac{1}{M_c} - \frac{1}{M} \right) \quad (24)$$

$$n_T = \left(\frac{\partial \ln T}{\partial \ln P_c} \right)_{P_c/P} = \frac{R}{M c_p} \left[1 - \left(\frac{\partial \ln M}{\partial \ln T} \right)_P \right] - \frac{R}{c_p M_c} \quad (25)$$

$$n_\epsilon = \left(\frac{\partial \ln \epsilon}{\partial \ln P_c} \right)_{P_c/P} = (n_{A/w})_e - (n_{A/w})_t \quad (26)$$

where

$$n_{A/w} = \left(\frac{\partial \ln A/w}{\partial \ln P_c} \right)_{P_c/P} = - \frac{R}{c_p M_c} \left[1 - \left(\frac{\partial \ln M}{\partial \ln T} \right)_P \right] - \frac{1}{\gamma} - n_I$$

$$n_{c^*} = \frac{\partial \ln c^*}{\partial \ln P_c} = 1 + (n_{A/w})_t \quad (27)$$

$$n_{I_{vac}} = \left(\frac{\partial \ln I_{vac}}{\partial \ln P_c} \right)_{P_c/P} = \frac{I(n_I - n_{c^*} - n_\epsilon)}{I_{vac}} + n_{c^*} + n_\epsilon \quad (28)$$

Equations (24) to (28) may be written in the approximate form:

$$I = I_1 \left(\frac{P_c}{P_{c,1}} \right)^{n_{I,1}} \quad (29)$$

$$T = T_1 \left(\frac{P_c}{P_{c,1}} \right)^{n_{T,1}} \quad (30)$$

$$\epsilon = \epsilon_1 \left(\frac{P_c}{P_{c,1}} \right)^{n_{\epsilon,1}} \quad (31)$$

$$c^* = c_1^* \left(\frac{P_c}{P_{c,1}} \right)^{n_{c^*,1}} \quad (32)$$

$$I_{vac} = I_{vac,1} \left(\frac{P_c}{P_{c,1}} \right)^{n_{I_{vac},1}} \quad (33)$$

where $P_{c,1}$ may be either 60, 150, 300, or 600 pounds per square inch absolute provided that I_1 , T_1 , ϵ_1 , c_1^* , $I_{vac,1}$, and their derivatives are the corresponding values for the chamber pressure selected.

The exponents obtained by means of equations (24) to (28) are shown in table III.

In order to illustrate the use of these derivatives, suppose it is desired to obtain the value of equilibrium specific impulse for a chamber pressure of 1200 pounds per square inch absolute and a pressure ratio of 81.65 (exit pressure, 1 atm) for an equivalence ratio R of 0.90 ($O/F = 7.143$): From table III, the value of I at this pressure ratio and equivalence ratio (but for a chamber pressure of 600 lb/sq in. abs) is 376.8 and the value of n_I is 0.0079. From equation (29),

$$\begin{aligned}
 I &= 376.8 \left(\frac{1200}{600} \right)^{0.0079} \\
 &= 376.8(1.0055) \\
 &= 378.9
 \end{aligned}$$

A comparison of the parameters obtained by means of the chamber-pressure correlation and by a direct calculation is given in the following table (R = 0.90, equilibrium composition during expansion):

Parameter	Chamber pressure, P_c , 1200 lb/sq in. abs; Exit pressure, P , 1 atm		
	Estimated by correlation	Direct calculation	Error
I	378.93	378.86	0.07
T_c	3623.3	3622.0	1.3
T_e	2338.4	2338.6	.2
ϵ	11.769	11.755	.014
c^*	7306.1	7304.7	1.4

It is expected that values estimated for other equivalence ratios and pressure ratios for chamber pressures from about 30 to 1200 pounds per square inch absolute will have small errors of the order of magnitude shown in the previous table.

The following analytic expressions were derived for equilibrium composition which permit exponents to be computed similar to those in equations (24) to (28) but for constant area ratio rather than constant pressure ratio (eqs. 34, 37, 38, 40):

$$\left(\frac{\partial \ln P_c/P}{\partial \ln P_c} \right)_{\epsilon} = n_{\epsilon} / \left(\frac{\partial \ln \epsilon}{\partial \ln P} \right)_s \quad (34)$$

where

$$\left(\frac{\partial \ln \epsilon}{\partial \ln P}\right)_s = -\frac{1}{\gamma} - \left(\frac{\partial \ln I}{\partial \ln P}\right)_s \quad (35)$$

and

$$\left(\frac{\partial \ln I}{\partial \ln P}\right)_s = -86.4554 \frac{T}{I^2 \mathcal{M}} \quad \text{or} \quad 1 - \frac{I_{\text{vac}}}{I} \quad (36)$$

$$\left(\frac{\partial \ln I}{\partial \ln P_c}\right)_\epsilon = n_I - \left(\frac{\partial \ln I}{\partial \ln P}\right)_s \left(\frac{\partial \ln P_c/P}{\partial \ln P_c}\right)_\epsilon \quad (37)$$

$$\left(\frac{\partial \ln T}{\partial \ln P_c}\right)_\epsilon = n_T - \left(\frac{\partial \ln T}{\partial \ln P}\right)_s \left(\frac{\partial \ln P_c/P}{\partial \ln P_c}\right)_\epsilon \quad (38)$$

where

$$\left(\frac{\partial \ln T}{\partial \ln P}\right)_s = \frac{\mathcal{R}}{\mathcal{M} c_p} \left[1 - \left(\frac{\partial \ln \mathcal{M}}{\partial \ln T}\right)_P \right] \quad (39)$$

$$\begin{aligned} \left(\frac{\partial \ln I_{\text{vac}}}{\partial \ln P_c}\right)_\epsilon &= n_{I_{\text{vac}}} - \left(\frac{\partial \ln I_{\text{vac}}}{\partial \ln P}\right)_s \left(\frac{\partial \ln P_c/P}{\partial \ln P_c}\right)_\epsilon \quad (40) \\ &= \frac{I(n_I - n_{c^*})}{I_{\text{vac}}} + n_{c^*} \end{aligned}$$

where

$$\left(\frac{\partial \ln I_{\text{vac}}}{\partial \ln P}\right)_s = \left(\frac{\partial \ln \epsilon}{\partial \ln P}\right)_s \left(1 - \frac{I}{I_{\text{vac}}}\right) \quad (41)$$

Data for constant area ratios for chamber pressures other than those given in this report may be obtained in a manner similar to the previous example by interpolating the data in table II (see, for example, fig. 7) together with exponents obtained from equations (34) to (41).

Effect of Finite Chamber Area

The use of a combustion chamber of finite cross-sectional area leads to a pressure change during the combustion process. For a cylindrical

chamber, the injector face pressure P_{in} may be found from the following equation derived from the conservation of the momentum

$$P_{in} = P_1 + \frac{W}{A_1 g_c} (V_1 - V_{in}) \quad (42)$$

where P_1 and V_1 are the static pressure and velocity at the nozzle entrance, respectively, and V_{in} is the average velocity of propellant (liquid or gas) in the axial direction when injected. Equation (42) may be written

$$P_{in} = P_c \left(\frac{P_1}{P_c} \right) (I_1 g_c - V_{in}) \quad (43)$$

where P_c is the stagnation pressure in the nozzle.

In order to illustrate this, consider a rocket operating at an equivalence ratio of 1.00, a nozzle stagnation pressure of 600 pounds per square inch absolute, a ratio of chamber area to throat area ϵ of 2.122, and $V_{in} = 100$ feet per second. From table II, corresponding to an area ratio of 2.122, P_c/P_1 is 1.05 and I is 43.3. From table V, c^* is 7039. Therefore, for these conditions, using equation (43),

$$\begin{aligned} P_{in} &= 600 \left(\frac{1}{1.05} \right) + \frac{600}{7039(2.122)} [(43.3)(32.17) - 100] \\ &= 571.4 + 51.9 \\ &= 623.3 \text{ lb/sq in. abs} \end{aligned}$$

SUMMARY OF RESULTS

A theoretical investigation of the performance of liquid hydrogen with liquid oxygen was made for the following conditions: (1) equilibrium and frozen composition during expansion, (2) four chamber pressures (60, 150, 300, and 600 lb/sq in. abs), (3) wide range of oxidant-fuel weight ratios (1.190 to 39.683), and (4) wide range of pressure ratios (1 to 4000).

1. The maximum values of specific impulse for expansion to 1 atmosphere are summarized in the following table:

Chamber pressure, P_c , lb/sq in. abs	Ratio of chamber pressure to exit pressure, P_c/P	Specific impulse, I, (lb)(sec)/lb	
		Equilibrium composition	Frozen composition
60	4.083	255.4	254.6
150	10.207	315.0	313.1
300	20.414	348.1	345.8
600	40.827	374.5	371.8

The maximum value of specific impulse for a chamber pressure of 600 pounds per square inch absolute and a pressure ratio of 4000 is 467.4 and 454.9 assuming equilibrium and frozen composition, respectively.

2. The difference between maximum values of specific impulse due to the assumption of equilibrium or frozen composition during expansion is less than 2 percent for pressure ratios up to 100 and about 3 to 4 percent for a pressure ratio of 4000.

3. For the same oxidant-fuel ratios, the difference between values of specific impulse due to the assumption of equilibrium or frozen composition during expansion may be as high as 15.8 percent for the conditions in this report.

Lewis Research Center
National Aeronautics and Space Administration
Cleveland, Ohio, March 2, 1959

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TABLE I. - PROPERTIES OF LIQUID PROPELLANTS

Properties	Hydrogen	Oxygen
Molecular weight, M	2.016	32.00
Density, g/cc	^a 0.0709 (at -252.7° C)	^b 1.1414 (at -182.0° C)
Freezing point, °C	^c -259.20	^c -218.76
Boiling point, °C	^c -252.77	^c -182.97
Enthalpy required to convert liquid at boiling point to gaseous elements at 25° C, kcal/mole	^d 1.894	^d 3.081
Enthalpy of vaporization, kcal/mole	^c 0.216 (at -252.77° C)	^c 1.630 (at -182.97° C)
Enthalpy of fusion, kcal/mole	^c 0.028 (at -259.20° C)	^c 0.106 (at -218.76° C)

^aRef. 23.^bRef. 24.^cRef. 7.^dRef. 1.

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Table with multiple sections for different equivalence ratios (R = 0.600, 0.700, 0.800, 0.900). Each section includes columns for Pressure ratio (Pc/P), Static pressure (P), Temperature (T), Enthalpy (h), Molecular weight (M), Isentropic exponent (γ), Specific heat (cp), Viscosity (μ), Thermal conductivity (k), Mach number (M), Specific impulse in vacuum (Isp), Area ratio (E), Thrust coefficient (Ct), and Specific impulse (I). Data is organized into sub-tables for each R value, with pressure ratios ranging from 1.00 to 4000.00.

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb/sq.in. abs.	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb)(sec)/lb	Area ratio, ϵ	Thrust coefficient, C_F	Specific impulse, I , (lb)(sec)/lb
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	60.00	2347	1054.4	26.257	1.1871	0.5285	798	0.00050	0.000	307.2	2.185	0.000	0.0
1.05	57.14	2390	1045.8	26.265	1.1885	0.5277	798	0.00049	0.287	195.1	1.260	0.204	27.4
1.20	50.00	2282	1022.5	26.286	1.1925	0.5273	784	0.00047	0.557	154.1	1.061	0.388	52.7
1.40	42.86	2228	996.2	26.307	1.1972	0.5265	772	0.00045	0.760	124.0	1.009	0.524	71.2
1.60	37.50	2180	974.0	26.323	1.2013	0.5272	761	0.00044	0.902	109.2	1.009	0.616	83.6
1.78	33.79	2143	957.0	26.334	1.2046	0.5267	753	0.00042	1.000	100.5	1.000	0.742	92.1
2.00	30.00	2101	937.9	26.345	1.2084	0.5269	743	0.00041	1.103	94.1	1.009	0.742	100.7
4.00	15.00	1898	834.6	26.387	1.2292	0.5102	689	0.00035	1.599	68.3	1.297	1.019	130.3
4.08	14.70	1891	831.7	26.388	1.2298	0.5092	685	0.00034	1.612	68.0	1.311	1.026	139.2
10.00	6.00	1556	717.0	26.403	1.2503	0.5069	606	0.00029	2.146	40.1	2.192	1.263	171.3
20.00	3.00	1351	641.3	26.406	1.2627	0.5019	547	0.00025	2.537	21.9	3.439	1.397	189.6
40.00	1.50	1167	575.7	26.406	1.2738	0.5001	491	0.00022	2.926	12.8	5.518	1.504	204.1
100.00	0.60	954	502.6	26.406	1.2893	0.5004	422	0.00018	3.452	6.3	10.507	1.615	219.1
200.00	0.30	815	456.7	26.406	1.3020	0.5006	372	0.00016	3.870	3.9	17.236	1.681	228.0
400.00	0.15	692	417.5	26.406	1.3121	0.5007	326	0.00013	4.314	2.5	26.358	1.735	235.4
1000.00	0.06	553	374.8	26.406	1.3329	0.5013	270	0.00011	4.991	1.5	54.842	1.792	243.2
2000.00	0.03	464	348.3	26.406	1.3428	0.5009	232	0.00009	5.484	0.9	90.278	1.827	247.9
4000.00	0.02	387	326.2	26.406	1.3563	0.5005	197	0.00008	6.070	0.6	148.471	1.855	251.7
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	60.00	2062	855.0	27.299	1.2228	0.4109	740	0.00037	0.000	282.2	2.186	0.000	0.0
1.05	57.14	2044	847.7	27.302	1.2242	0.4079	736	0.00037	0.283	178.9	1.269	0.204	25.2
1.20	50.00	1995	828.1	27.309	1.2260	0.4004	724	0.00036	0.550	154.7	1.061	0.392	48.4
1.40	42.86	1938	808.0	27.316	1.2323	0.3925	710	0.00034	0.751	139.3	1.066	0.529	65.3
1.60	37.50	1890	787.4	27.321	1.2376	0.3864	698	0.00033	0.892	124.7	1.011	0.621	76.7
1.80	33.40	1849	771.7	27.324	1.2397	0.3818	688	0.00033	1.000	119.9	1.000	0.690	85.1
2.00	30.00	1811	757.4	27.327	1.2414	0.3775	679	0.00032	1.093	114.3	1.007	0.747	92.2
4.00	15.00	1576	674.1	27.336	1.2520	0.3579	617	0.00026	1.594	80.7	1.282	1.022	126.2
4.08	14.70	1571	669.7	27.336	1.2520	0.3575	613	0.00026	1.607	80.1	1.295	1.029	127.0
10.00	6.00	1304	576.3	27.338	1.2707	0.3415	539	0.00023	2.151	48.2	2.145	1.261	155.7
20.00	3.00	1122	515.3	27.339	1.2819	0.3309	484	0.00020	2.549	26.6	3.345	1.393	171.9
40.00	1.50	961	462.9	27.339	1.2928	0.3209	432	0.00018	2.946	14.2	5.334	1.496	184.7
100.00	0.60	778	405.1	27.339	1.3094	0.3076	367	0.00015	3.486	8.3	10.072	1.603	197.8
200.00	0.30	659	369.0	27.339	1.3227	0.2979	321	0.00012	3.918	4.8	16.410	1.666	205.6
400.00	0.15	555	338.5	27.339	1.3364	0.2888	279	0.00011	4.379	3.3	26.810	1.717	212.0
1000.00	0.06	438	305.6	27.339	1.3536	0.2783	230	0.00008	5.047	2.0	51.370	1.771	218.6
2000.00	0.03	365	285.4	27.339	1.3632	0.2728	192	0.00007	5.611	1.4	84.029	1.804	222.6
4000.00	0.02	303	268.6	27.339	1.3697	0.2693	164	0.00006	6.234	1.0	137.526	1.830	225.9

C O N T I N U E

C O N T I N U E

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OX/GEN [Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Table with 14 columns: Pressure ratio, Static pressure, Temperature, Enthalpy, Molecular weight, Isentropic exponent, Specific heat, Viscosity, Thermal conductivity, Mach number, Specific impulse, Area ratio, Thrust coefficient, Specific impulse. The table is organized into sections for different equivalence ratios: R = 0.600, R = 0.700, R = 0.800, and R = 0.900. Each section contains data for pressure ratios from 1.00 to 4.00, and then 10.00, 20.00, 100.00, 200.00, 1000.00, and 4000.00.

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P, lb./sq. in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{sp} , lb.(sec)/lb.	Area ratio, E	Thrust coefficient, C_f	Specific impulse, I , lb.(sec)/lb.
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	150.00	2363	1054.4	26.287	1.1944	0.5005	802	0.0004	0.000			0.000	0.0
1.05	142.86	2344	1045.7	26.294	1.1957	.4958	798	.0004	.286	308.0	2.169	.202	27.5
1.20	125.00	2295	1022.3	26.311	1.1994	.4833	787	.0004	.556	195.6	1.261	.389	52.8
1.40	107.14	2238	995.9	26.328	1.2037	.4699	774	.0004	.758	174.4	1.062	.525	71.3
1.60	93.75	2188	973.6	26.341	1.2075	.4590	763	.0004	.900	169.5	1.010	.617	83.8
1.78	84.31	2149	956.3	26.350	1.2105	.4509	754	.0004	1.000	168.7	1.000	.680	92.4
2.00	75.00	2107	937.5	26.359	1.2138	.4426	745	.0004	1.101	169.4	1.009	.743	100.9
4.00	37.50	1859	834.0	26.391	1.2322	.4044	685	.0003	1.999	162.4	1.020	1.020	138.5
10.00	15.00	1555	716.5	26.404	1.2512	.3757	605	.0002	2.148	101.2	2.187	1.263	171.5
10.21	14.70	1549	714.1	26.404	1.2515	.3752	604	.0002	2.160	101.5	2.215	1.267	172.1
20.00	7.50	1350	640.8	26.406	1.2629	.3616	547	.0002	2.539	113.0	3.431	1.597	189.7
40.00	3.75	1166	575.3	26.406	1.2739	.3500	491	.0002	2.928	122.9	5.906	1.904	204.2
100.00	1.50	953	502.5	26.406	1.2894	.3353	421	.0001	3.455	133.4	10.485	1.614	217.2
200.00	.75	814	456.5	26.406	1.3021	.3244	372	.0001	3.873	139.8	17.201	1.680	228.1
400.00	.38	691	417.3	26.406	1.3192	.3140	326	.0001	4.317	145.1	28.301	1.734	235.5
1000.00	.15	552	374.6	26.406	1.3330	.3012	270	.0001	4.955	150.6	54.731	1.791	243.2
2000.00	.08	463	348.1	26.406	1.3459	.2925	234	.0000	5.487	154.0	90.095	1.826	247.9
4000.00	.04	387	326.0	26.406	1.3563	.2864	197	.0000	6.075	156.8	148.169	1.854	251.7
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	150.00	2066	855.0	27.307	1.2269	0.4020	741	0.0003	0.000			0.000	0.0
1.05	142.86	2048	847.7	27.310	1.2282	.3996	737	.0003	.283	262.4	2.188	.204	25.2
1.20	125.00	1998	828.0	27.310	1.2315	.3934	725	.0003	.549	179.0	1.269	.392	48.4
1.40	107.14	1941	805.9	27.321	1.2355	.3869	711	.0003	.750	159.3	1.066	.529	65.3
1.60	93.75	1892	787.3	27.325	1.2384	.3818	699	.0003	.891	154.8	1.011	.622	76.7
1.80	83.45	1850	771.5	27.327	1.2410	.3777	688	.0003	1.000	153.2	1.000	.690	85.2
2.00	75.00	1812	757.3	27.329	1.2435	.3742	679	.0003	1.092	154.4	1.007	.747	92.2
4.00	37.50	1578	672.0	27.337	1.2565	.3570	617	.0002	1.994	165.7	1.281	1.022	126.2
10.00	15.00	1303	576.2	27.338	1.2708	.3411	539	.0002	2.152	182.2	2.144	1.262	155.7
10.21	14.70	1298	574.3	27.338	1.2711	.3408	538	.0002	2.164	182.5	2.171	1.266	156.3
20.00	7.50	1122	515.2	27.339	1.2815	.3309	484	.0002	2.550	192.6	3.443	1.393	171.9
40.00	3.75	961	462.8	27.339	1.2929	.3209	432	.0001	2.947	201.2	5.332	1.496	184.7
100.00	1.50	778	405.1	27.339	1.3094	.3076	367	.0001	3.487	210.3	10.068	1.603	197.9
200.00	.75	658	369.0	27.339	1.3227	.2979	321	.0001	3.919	215.8	16.403	1.666	205.6
400.00	.38	554	338.5	27.339	1.3364	.2887	279	.0001	4.380	220.3	26.799	1.717	212.0
1000.00	.15	438	305.6	27.339	1.3556	.2782	229	.0000	5.048	225.0	51.350	1.771	218.7
2000.00	.08	365	285.4	27.339	1.3652	.2728	195	.0000	5.612	227.8	83.996	1.803	222.6
4000.00	.04	303	268.6	27.339	1.3697	.2693	164	.0000	6.235	230.1	137.472	1.830	225.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Combustion-chamber pressure, 500 pounds per square inch absolute; equilibrium composition during isentropic expansion

Table with 14 columns: Pressure ratio, Static pressure, Temperature, Enthalpy, Molecular weight, Isentropic exponent, Specific heat, Viscosity, Thermal conductivity, Mach number, Specific impulse, Area ratio, Thrust coefficient, Specific impulse. Data is organized into sections for R = 0.150, 0.200, 0.250, and 0.300, each with a corresponding O/F ratio.

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb/sq.in. abs.	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb-sec/lb	Area ratio, ϵ	Thrust coefficient, C_f	Specific impulse, I , lb-sec/lb
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	300.00	2372	1054.4	26.307	1.1993	0.4836	804	0.00046	0.000	0.000		0.000	0.0
1.05	285.71	2354	1045.7	26.312	1.2005	0.4796	800	0.00046	0.286	308.5	2.172	0.203	27.5
1.20	250.00	2303	1022.2	26.327	1.2040	0.4609	789	0.00044	0.355	195.0	1.262	0.390	22.9
1.40	214.29	2244	995.8	26.341	1.2080	0.4574	776	0.00043	0.757	174.5	1.053	0.526	21.4
1.60	187.50	2194	973.4	26.352	1.2115	0.4481	765	0.00041	0.899	169.7	1.010	0.618	20.9
1.78	168.42	2153	955.8	26.360	1.2143	0.4412	755	0.00040	1.000	168.9	1.000	0.662	20.6
2.00	150.00	2110	937.2	26.367	1.2173	0.4341	745	0.00039	1.100	169.5	1.009	0.743	20.1
4.00	75.00	1859	833.7	26.394	1.2340	0.4010	685	0.00034	1.599	182.5	1.294	1.020	13.6
10.00	30.00	1555	716.2	26.404	1.2517	0.3749	605	0.00028	2.149	201.2	2.184	1.265	12.6
20.00	15.00	1349	640.5	26.406	1.2631	0.3614	547	0.00025	2.541	213.0	3.426	1.397	10.9
20.41	14.70	1343	638.5	26.406	1.2634	0.3611	545	0.00025	2.552	213.4	3.474	1.400	10.2
40.00	7.50	1165	575.1	26.406	1.2740	0.3499	491	0.00022	2.930	222.9	5.499	1.503	20.2
100.00	3.00	952	502.2	26.406	1.2895	0.3352	421	0.00018	3.457	235.4	10.472	1.614	21.2
200.00	1.50	813	456.3	26.406	1.3021	0.3243	372	0.00016	3.875	239.8	17.179	1.679	22.1
400.00	0.75	690	417.1	26.406	1.3153	0.3139	325	0.00013	4.319	245.1	28.266	1.735	23.5
1000.00	0.30	552	374.5	26.406	1.3331	0.3012	270	0.00011	4.957	250.7	54.663	1.791	24.2
2000.00	0.15	463	348.0	26.406	1.3459	0.2928	232	0.00009	5.490	254.0	89.984	1.823	24.9
4000.00	0.08	386	326.0	26.406	1.3564	0.2864	197	0.00007	6.077	256.8	147.985	1.853	25.1
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	300.00	2059	855.0	27.313	1.2295	0.3968	742	0.00036	0.000	0.000		0.000	0.0
1.05	285.71	2051	847.7	27.315	1.2306	0.3947	737	0.00036	0.282	282.5	2.189	0.209	25.2
1.20	250.00	2000	828.0	27.319	1.2337	0.3893	725	0.00035	0.548	179.1	1.270	0.393	22.5
1.40	214.29	1942	805.9	27.324	1.2371	0.3835	711	0.00034	0.749	159.4	1.066	0.529	20.4
1.60	187.50	1893	787.3	27.327	1.2400	0.3790	699	0.00033	0.891	154.8	1.011	0.622	20.8
1.80	168.42	1851	771.4	27.329	1.2424	0.3753	689	0.00032	1.000	153.9	1.000	0.691	20.3
2.00	150.00	1813	757.2	27.331	1.2445	0.3722	679	0.00031	1.092	154.4	1.007	0.747	22.2
4.00	75.00	1578	671.9	27.337	1.2567	0.3584	617	0.00028	1.594	165.8	1.281	1.022	12.6
10.00	30.00	1303	576.1	27.339	1.2709	0.3411	539	0.00023	2.152	182.2	2.143	1.262	15.8
20.00	15.00	1122	515.1	27.339	1.2815	0.3309	484	0.00020	2.550	192.6	3.342	1.393	17.0
20.41	14.70	1117	513.5	27.339	1.2819	0.3306	482	0.00020	2.562	192.9	3.368	1.396	17.4
40.00	7.50	961	462.8	27.339	1.2929	0.3209	432	0.00018	2.947	201.2	5.330	1.496	18.7
100.00	3.00	777	405.0	27.339	1.3095	0.3076	367	0.00015	3.487	210.3	10.066	1.603	19.9
200.00	1.50	658	368.9	27.339	1.3227	0.2979	321	0.00012	3.919	215.8	16.399	1.666	20.7
400.00	0.75	554	336.5	27.339	1.3364	0.2887	279	0.00011	4.380	220.3	26.792	1.717	21.0
1000.00	0.30	448	305.5	27.339	1.3536	0.2782	229	0.00008	5.049	225.0	51.338	1.771	21.7
2000.00	0.15	365	285.3	27.339	1.3733	0.2728	195	0.00007	5.613	227.8	83.976	1.803	22.6
4000.00	0.08	303	266.6	27.339	1.3977	0.2693	164	0.00006	6.235	230.1	137.459	1.830	23.9

CONT.

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb./sq. in. abs.	Temperature, T , °K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse, I_{vac} , (lb)(sec)/lb	Area ratio, ϵ	Thrust coefficient, C_f	Specific impulse, I , (lb)(sec)/(lb)
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	600.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000	530.0	2.250	0.000	0.0
1.05	571.43	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	0.271	530.0	2.250	0.210	47.4
1.20	500.00	1129	5218.6	4.416	1.3436	1.7597	303	0.00070	0.527	534.2	1.297	0.403	90.8
1.40	428.57	1085	5141.8	4.416	1.3469	1.7472	293	0.00068	0.722	536.1	1.081	0.543	122.2
1.60	375.00	1049	5077.7	4.416	1.3497	1.7370	285	0.00066	0.860	536.6	1.018	0.636	143.2
1.87	321.68	1008	5006.8	4.416	1.3528	1.7256	276	0.00063	1.000	534.1	1.000	0.725	163.4
2.00	300.00	989	4975.4	4.416	1.3541	1.7210	272	0.00062	1.059	528.4	1.003	0.761	171.5
4.00	150.00	824	4693.4	4.416	1.3651	1.6824	234	0.00052	1.566	301.7	1.233	1.031	232.3
10.00	60.00	643	4392.5	4.416	1.3748	1.6506	188	0.00042	2.152	327.5	1.974	1.257	283.1
20.00	30.00	532	4209.8	4.416	1.3799	1.6345	159	0.00035	2.586	343.5	2.983	1.376	309.9
40.00	15.00	439	4058.9	4.416	1.3824	1.6269	133	0.00029	3.031	356.4	4.620	1.467	330.4
40.83	14.70	437	4054.8	4.416	1.3824	1.6267	132	0.00029	3.044	356.8	4.682	1.469	330.9
100.00	6.00	340	3899.0	4.416	1.3883	1.6089	104	0.00023	3.648	369.8	8.432	1.558	350.8
200.00	3.00	280	3802.6	4.416	1.3930	1.5951	85	0.00018	4.148	377.7	13.431	1.610	362.6
400.00	1.50	230	3723.2	4.416	1.4069	1.5558	70	0.00015	4.674	384.1	21.488	1.652	372.0
1000.00	0.60	175	3640.1	4.416	1.4347	1.4892	55	0.00011	5.438	390.6	39.928	1.694	381.6
2000.00	0.30	142	3590.9	4.416	1.4552	1.4387	45	0.00009	6.096	394.3	63.572	1.719	387.2
4000.00	0.15	114	3551.2	4.416	1.4717	1.4039	36	0.00007	6.842	397.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	600.00	1514	2969.7	5.216	1.3078	1.6187	402	0.00084	0.000	552.1	2.233	0.000	0.0
1.05	571.43	1497	2941.7	5.216	1.3089	1.6143	399	0.00083	0.274	552.1	2.233	0.209	49.3
1.20	500.00	1450	2866.8	5.216	1.3119	1.6024	389	0.00081	0.533	548.6	1.289	0.400	94.6
1.40	428.57	1399	2785.1	5.216	1.3154	1.5888	378	0.00078	0.730	549.3	1.077	0.539	127.4
1.60	375.00	1354	2713.2	5.216	1.3185	1.5773	369	0.00076	0.869	549.6	1.016	0.632	149.4
1.87	324.94	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	547.3	1.000	0.716	169.2
2.00	300.00	1282	2601.1	5.216	1.3236	1.5584	353	0.00072	1.068	547.8	1.004	0.757	179.1
4.00	150.00	1079	2290.0	5.216	1.3391	1.5046	307	0.00061	1.572	316.7	1.244	1.029	243.2
10.00	60.00	852	1954.3	5.216	1.3558	1.4516	251	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	30.00	709	1748.8	5.216	1.3656	1.4232	213	0.00040	2.573	362.0	3.049	1.379	325.9
40.00	15.00	588	1578.0	5.216	1.3715	1.4066	179	0.00034	3.010	376.0	4.739	1.472	348.0
40.83	14.70	585	1573.4	5.216	1.3716	1.4062	178	0.00034	3.023	376.4	4.802	1.474	348.6
100.00	6.00	458	1396.3	5.216	1.3770	1.3916	142	0.00026	3.619	390.5	8.679	1.565	370.0
200.00	3.00	379	1286.1	5.216	1.3811	1.3808	117	0.00022	4.111	399.1	13.870	1.619	382.7
400.00	1.50	312	1195.2	5.216	1.3858	1.3684	96	0.00016	4.638	406.1	22.296	1.662	393.0
1000.00	0.60	242	1098.9	5.216	1.3972	1.3402	74	0.00013	5.394	413.4	41.979	1.706	403.5
2000.00	0.30	198	1041.1	5.216	1.4157	1.2976	61	0.00011	6.014	417.7	67.687	1.733	409.7
4000.00	0.15	161	993.9	5.216	1.4362	1.2543	50	0.00009	6.701	421.1	108.754	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	600.00	1817	1249.3	6.016	1.2827	1.4998	481	0.00092	0.000	563.4	2.218	0.000	0.0
1.05	571.43	1797	1220.2	6.016	1.2837	1.4955	477	0.00091	0.276	563.4	2.218	0.207	50.3
1.20	500.00	1745	1142.1	6.016	1.2865	1.4840	467	0.00089	0.538	556.2	1.283	0.398	96.6
1.40	428.57	1686	1054.7	6.016	1.2896	1.4712	456	0.00086	0.736	556.3	1.073	0.536	130.1
1.60	375.00	1636	981.5	6.016	1.2924	1.4604	446	0.00084	0.876	556.6	1.015	0.629	152.7
1.87	327.81	1587	909.9	6.016	1.2952	1.4494	436	0.00081	1.000	554.5	1.000	0.708	171.8
2.00	300.00	1555	863.9	6.016	1.2971	1.4423	429	0.00080	1.076	551.1	1.005	0.754	183.1
4.00	150.00	1322	535.1	6.016	1.3125	1.3874	378	0.00068	1.578	325.5	1.256	1.027	249.3
10.00	60.00	1057	1764.1	6.016	1.3329	1.3225	314	0.00054	2.147	355.3	2.048	1.258	305.6
20.00	30.00	887	9954.0	6.016	1.3460	1.2849	269	0.00046	2.563	373.7	3.127	1.382	335.7
40.00	15.00	741	9768.1	6.016	1.3568	1.2560	228	0.00038	2.987	388.7	4.883	1.478	359.0
40.83	14.70	737	9763.1	6.016	1.3571	1.2552	227	0.00038	3.000	389.1	4.949	1.481	359.6
100.00	6.00	581	9569.0	6.016	1.3663	1.2321	181	0.00030	3.581	404.2	8.985	1.575	382.4
200.00	3.00	482	9447.8	6.016	1.3717	1.2189	151	0.00025	4.064	413.4	14.396	1.630	395.9
400.00	1.50	399	9347.3	6.016	1.3755	1.2100	125	0.00020	4.582	420.9	23.208	1.675	406.8
1000.00	0.60	310	9240.5	6.016	1.3820	1.1949	95	0.00015	5.327	428.7	43.893	1.722	418.1
2000.00	0.30	256	9175.9	6.016	1.3885	1.1810	78	0.00012	5.945	433.4	71.279	1.749	424.7
4000.00	0.15	210	9122.7	6.016	1.4037	1.1485	64	0.00010	6.606	437.2	115.650	1.771	430.2
R = 0.300, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	600.00	2094	9932.7	6.815	1.2613	1.4145	551	0.00098	0.000	568.6	2.206	0.000	0.0
1.05	571.43	2073	9903.1	6.815	1.2623	1.4097	547	0.00097	0.279	568.6	2.206	0.206	50.8
1.20	500.00	2016	9823.5	6.815	1.2650	1.3967	537	0.00095	0.542	559.8	1.277	0.396	97.5
1.40	428.57	1952	9734.3	6.815	1.2681	1.3825	525	0.00092	0.742	549.8	1.071	0.533	131.4
1.60	375.00	1898	9659.4	6.816	1.2708	1.3706	515	0.00089	0.882	540.3	1.013	0.626	154.2
1.87	330.21	1847	9589.9	6.816	1.2734	1.3598	505	0.00087	1.000	538.3	1.000	0.701	172.7
2.00	300.00	1809	9538.8	6.816	1.2753	1.3519	498	0.00085	1.082	539.1	1.006	0.751	185.1
4.00	150.00	1553	9199.6	6.816	1.2894	1.2991	445	0.00074	1.585	330.6	1.266	1.025	252.6
10.00	60.00	1257	8825.3	6.816	1.3095	1.2336	375	0.00060	2.148	361.8	2.085	1.260	310.4
20.00	30.00	1064	8591.1	6.816	1.3248	1.1891	325	0.00051	2.555	381.2	3.206	1.386	341.7
40.83	14.70	891	8388.2	6.816	1.3388	1.1522	277	0.00042	2.981	397.4	5.106	1.488	366.6
40.00	15.00	895	8393.6	6.816	1.3384	1.1531	279	0.00042	2.968	397.0	5.037	1.485	366.0
100.00	6.00	707	8180.3	6.816	1.3530	1.1174	223	0.00033	3.544	413.5	9.324	1.585	390.5
200.00	3.00	590	8049.6	6.816	1.3603	1.1007	187	0.00027	4.013	423.3	14.993	1.643	404.8
400.00	1.50	490	7940.8	6.816	1.3666	1.0867	156	0.00023	4.517	431.3	24.234	1.689	416.3
1000.00	0.60	383	7824.8	6.816	1.3723	1.0746	120	0.00017	5.247	439.6	45.999	1.738	428.3
2000.00	0.30	317	7754.3	6.816	1.3775	1.0638	98	0.00014	5.852	444.6	74.912	1.767	435.4
4000.00	0.15	262	7696.0	6.816	1.3827	1.0534	80	0.00011	6.510	448.7	122.185	1.790	441.2

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P_s , lb/in ² abs	Temperature, T_c , °K	Enthalpy, h_c , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb)(sec)/lb	Area ratio, ϵ	Thrust coefficient, C_f	Specific impulse, I , (lb)(sec)/lb
R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	600.00	2347	8892.8	7.610	1.2410	1.3691	611	0.00104	0.000	570.0	2.195	0.000	0.0
1.05	571.43	2325	8863.0	7.610	1.2421	1.3521	608	0.00103	0.281	561.0	1.273	0.205	50.9
1.20	500.00	2266	8783.0	7.611	1.2451	1.3440	598	0.00100	0.486	546.0	1.068	0.598	91.7
1.40	428.57	2198	8693.2	7.613	1.2485	1.3249	586	0.00097	0.747	521.2	0.861	0.931	131.8
1.60	375.00	2140	8617.6	7.613	1.2513	1.3099	576	0.00094	0.987	511.8	0.712	0.623	194.7
1.81	332.36	2089	8551.7	7.614	1.2538	1.2974	567	0.00092	1.000	510.0	0.600	0.695	172.5
2.00	300.00	2046	8495.7	7.614	1.2559	1.2874	559	0.00090	1.088	510.9	0.507	0.749	185.9
4.00	150.00	1771	8150.9	7.616	1.2699	1.2291	506	0.00079	1.590	333.2	1.275	1.023	254.1
10.00	60.00	1451	7766.6	7.616	1.2885	1.1655	434	0.00065	2.149	365.6	2.119	1.261	313.0
20.00	30.00	1238	7523.9	7.616	1.3036	1.1204	381	0.00055	2.550	385.8	3.281	1.390	345.1
40.83	14.70	1045	7311.7	7.616	1.3192	1.0783	328	0.00046	2.965	402.9	5.260	1.694	370.9
40.00	15.00	1050	7317.3	7.616	1.3188	1.0794	330	0.00046	2.953	402.5	5.188	1.691	370.3
100.00	6.00	838	7092.4	7.616	1.3364	1.0365	267	0.00036	3.511	419.8	9.676	1.994	395.8
200.00	3.00	702	6953.5	7.616	1.3475	1.0118	225	0.00030	3.964	430.2	15.026	1.654	410.8
400.00	1.50	586	6837.3	7.616	1.3553	0.9953	188	0.00025	4.453	438.6	29.350	1.703	422.9
1000.00	0.60	460	6712.8	7.616	1.3634	0.9789	148	0.00019	5.162	447.5	48.288	1.754	435.5
2000.00	0.30	382	6636.9	7.616	1.3684	0.9692	121	0.00016	5.751	452.8	78.852	1.784	443.1
4000.00	0.15	317	6573.8	7.616	1.3738	0.9590	98	0.00013	6.392	457.2	128.949	1.809	449.2
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	600.00	2574	8050.5	8.396	1.2209	1.3697	663	0.00110	0.000	568.5	2.184	0.000	0.0
1.05	571.43	2552	8020.9	8.397	1.2220	1.3599	660	0.00109	0.283	568.5	1.208	0.204	50.7
1.20	500.00	2492	7941.2	8.401	1.2252	1.3344	650	0.00106	0.500	560.5	1.068	0.592	91.5
1.40	428.57	2422	7851.7	8.404	1.2289	1.3072	639	0.00102	0.752	521.0	0.861	0.928	131.5
1.60	375.00	2363	7776.1	8.408	1.2320	1.2856	630	0.00100	0.995	511.8	0.712	0.621	194.5
1.79	334.53	2313	7713.0	8.408	1.2347	1.2685	621	0.00097	1.000	510.2	0.600	0.688	171.4
2.00	300.00	2266	7654.1	8.410	1.2372	1.2533	613	0.00095	1.094	511.2	0.507	0.746	185.7
4.00	150.00	1978	7306.9	8.414	1.2520	1.1787	561	0.00083	1.594	334.5	1.274	1.022	254.4
10.00	60.00	1637	6916.6	8.416	1.2701	1.1109	489	0.00069	2.149	367.6	2.150	1.262	314.1
20.00	30.00	1408	6667.8	8.416	1.2842	1.0669	434	0.00059	2.545	388.6	3.351	1.395	346.9
40.00	15.00	1204	6454.3	8.416	1.2932	1.0253	380	0.00050	2.940	405.9	5.234	1.497	372.7
40.83	14.70	1199	6448.5	8.416	1.2996	1.0242	379	0.00050	2.951	406.3	5.409	1.500	373.4
100.00	6.00	970	6219.8	8.416	1.3188	0.9767	313	0.00040	3.482	424.1	10.029	1.603	399.1
200.00	3.00	818	6073.7	8.416	1.3318	0.9478	266	0.00033	3.920	435.0	16.282	1.666	414.7
400.00	1.50	687	5950.8	8.416	1.3428	0.9249	224	0.00027	4.391	443.9	26.525	1.717	427.4
1000.00	0.60	542	5818.5	8.416	1.3537	0.9037	176	0.00021	5.076	453.3	50.761	1.770	440.7
2000.00	0.30	452	5737.3	8.416	1.3595	0.8928	146	0.00017	5.648	459.0	83.105	1.802	448.6
4000.00	0.15	376	5669.9	8.416	1.3647	0.8835	119	0.00014	6.271	463.6	136.261	1.828	455.1
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	600.00	2773	7354.5	9.167	1.2018	1.4156	707	0.00119	0.000	565.0	2.172	0.000	0.0
1.05	571.43	2752	7325.3	9.170	1.2029	1.4027	704	0.00118	0.285	565.0	1.263	0.203	50.4
1.20	500.00	2692	7246.5	9.177	1.2060	1.3686	695	0.00114	0.504	538.6	1.063	0.590	96.9
1.40	428.57	2624	7157.9	9.184	1.2097	1.3318	685	0.00110	0.757	519.6	0.863	0.926	130.8
1.60	375.00	2565	7082.9	9.189	1.2128	1.3022	676	0.00106	0.999	510.7	0.713	0.618	153.7
1.78	336.72	2517	7023.8	9.193	1.2154	1.2799	669	0.00104	1.000	509.2	0.600	0.682	169.6
2.00	300.00	2467	6961.6	9.197	1.2183	1.2573	661	0.00101	1.100	510.3	0.509	0.743	184.9
4.00	150.00	2174	6614.5	9.210	1.2347	1.1514	611	0.00087	1.599	334.2	1.293	1.020	253.7
10.00	60.00	1817	6220.9	9.215	1.2537	1.0682	540	0.00072	2.149	368.3	2.182	1.263	314.1
20.00	30.00	1575	5967.7	9.216	1.2670	1.0237	485	0.00063	2.539	389.9	3.420	1.397	347.4
40.00	15.00	1357	5749.0	9.216	1.2811	0.9828	429	0.00054	2.927	407.8	5.446	1.503	373.8
40.83	14.70	1350	5743.0	9.216	1.2815	0.9816	428	0.00054	2.939	408.3	5.554	1.506	374.5
100.00	6.00	1104	5506.6	9.216	1.3008	0.9325	358	0.00043	3.455	426.8	10.381	1.612	401.0
200.00	3.00	937	5354.4	9.216	1.3152	0.8996	307	0.00036	3.879	438.3	16.950	1.678	417.2
400.00	1.50	792	5225.4	9.216	1.3282	0.8727	261	0.00030	4.334	447.7	27.755	1.731	430.4
1000.00	0.60	629	5085.6	9.216	1.3418	0.8465	207	0.00023	4.994	457.6	53.398	1.787	444.3
2000.00	0.30	526	4999.5	9.216	1.3502	0.8313	172	0.00019	5.544	463.6	87.714	1.820	452.7
4000.00	0.15	439	4927.5	9.216	1.3562	0.8210	142	0.00016	6.148	468.5	144.197	1.848	459.5
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	600.00	2944	6769.6	9.919	1.1849	1.5012	745	0.00130	0.000	559.8	2.162	0.000	0.0
1.05	571.43	2923	6741.0	9.923	1.1859	1.4856	742	0.00129	0.287	559.8	1.262	0.202	50.0
1.20	500.00	2866	6663.6	9.935	1.1835	1.4440	734	0.00124	0.508	535.7	1.068	0.588	96.1
1.40	428.57	2800	6576.3	9.947	1.1917	1.3979	724	0.00119	0.762	517.3	0.861	0.924	129.7
1.60	375.00	2742	6502.4	9.957	1.1946	1.3600	716	0.00115	0.904	508.6	0.713	0.616	152.5
1.77	338.88	2699	6447.5	9.963	1.1970	1.3324	710	0.00112	1.000	507.3	0.600	0.676	167.4
2.00	300.00	2647	6382.5	9.971	1.1998	1.3008	702	0.00109	1.106	508.6	0.510	0.741	183.5
4.00	150.00	2356	6037.6	9.999	1.2169	1.1551	655	0.00092	1.603	333.1	1.303	1.019	252.4
10.00	60.00	1990	5642.7	10.013	1.2378	1.0408	587	0.00076	2.147	368.0	2.216	1.264	313.1
20.00	30.00	1737	5386.6	10.015	1.2515	0.9888	532	0.00066	2.532	390.1	3.491	1.401	346.9
40.00	15.00	1507	5163.7	10.016	1.2647	0.9482	477	0.00057	2.914	408.6	5.620	1.509	373.8
40.83	14.70	1501	5157.7	10.016	1.2651	0.9471	475	0.00057	2.926	409.1	5.701	1.512	374.5
100.00	6.00	1238	4914.9	10.016	1.2834	0.8984	403	0.00046	3.431	428.3	10.736	1.622	401.7
200.00	3.00	1059	4757.3	10.016	1.2984	0.8534	350	0.00039	3.842	440.3	17.634	1.690	418.5
400.00	1.50	900	4622.8	10.016	1.3125	0.8333	300	0.00032	4.280	450.2	29.032	1.745	432.2
1000.00	0.60	720	4476.0	10.016	1.3291	0.8013	240	0.00025	4.914	460.7	56.203	1.804	446.7
2000.00	0.30	606	4385.0	10.016	1.3387	0.7841	201	0.00021	5.445	467.0	92.675	1.839	455.5
4000.00	0.15	507	4308.7	10.016	1.3473	0.7696	166	0.00017	6.024	472.2	152.844	1.868	462.7

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute, equilibrium composition during isentropic expansion

Pressure ratio, P _c /P _a	Static pressure, P _s , lb/sq in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, C_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb)(sec)/lb	Area ratio, ϵ	Thrust coefficient, C _f	Specific impulse, I, (lb)(sec)/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	600.00	3208	5841.6	11.347	1.1593	1.7671	803	0.00150	0.000	546.7	2.144	0.000	0.0
1.05	571.43	3189	5814.3	11.356	1.1598	1.7482	801	0.00158	0.291	546.7	2.144	0.290	48.8
1.20	500.00	3137	5740.5	11.379	1.1611	1.6966	794	0.00152	0.564	347.8	1.250	0.385	93.8
1.40	428.57	3077	5656.9	11.404	1.1629	1.6375	786	0.00146	0.770	310.8	1.057	0.520	124.8
1.60	375.00	3025	5586.0	11.425	1.1646	1.5869	779	0.00140	0.913	302.6	1.007	0.612	149.1
1.75	342.61	2990	5538.8	11.438	1.1659	1.5531	774	0.00137	1.000	301.5	1.000	0.666	162.3
2.00	300.00	2938	5470.4	11.457	1.1680	1.5041	766	0.00132	1.117	303.1	1.012	0.737	179.7
4.00	150.00	2669	5134.6	11.535	1.1817	1.2723	727	0.00108	1.613	328.7	1.323	1.017	248.0
10.00	60.00	2313	4742.5	11.593	1.2048	1.0538	667	0.00085	2.145	365.0	2.288	1.268	309.3
20.00	30.00	2050	4483.6	11.609	1.2216	0.9574	617	0.00072	2.517	388.2	3.644	1.410	343.7
40.00	15.00	1803	4255.3	11.615	1.2359	0.8996	564	0.00063	2.885	407.6	5.926	1.524	371.5
40.83	14.70	1796	4249.0	11.615	1.2363	0.8983	562	0.00063	2.896	408.2	6.013	1.527	372.3
100.00	6.00	1506	3996.4	11.616	1.2528	0.8482	490	0.00052	3.381	428.7	11.474	1.643	400.7
200.00	3.00	1306	3829.9	11.616	1.2663	0.8136	434	0.00045	3.772	441.6	19.054	1.716	418.4
400.00	1.50	1125	3686.0	11.616	1.2806	0.7807	379	0.00038	4.182	452.4	31.724	1.776	433.1
1000.00	0.60	916	3526.4	11.616	1.2996	0.7420	311	0.00030	4.769	464.0	62.274	1.841	448.8
2000.00	0.30	778	3426.2	11.616	1.3130	0.7177	264	0.00025	5.257	471.1	103.640	1.880	458.4
4000.00	0.15	658	3341.2	11.616	1.3245	0.6983	222	0.00020	5.791	476.9	172.288	1.913	466.4
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	600.00	3381	5138.3	12.664	1.1429	2.1301	846	0.00137	0.000	531.5	2.133	0.000	0.0
1.05	571.43	3364	5112.5	12.677	1.1430	2.1115	843	0.00135	0.293	531.5	2.133	0.199	47.4
1.20	500.00	3317	5042.7	12.711	1.1433	2.0594	837	0.00129	0.568	338.5	1.245	0.383	91.2
1.40	428.57	3265	4963.5	12.750	1.1438	1.9976	830	0.00122	0.775	302.7	1.054	0.517	123.3
1.60	375.00	3217	4898.2	12.782	1.1443	1.9428	823	0.00117	0.920	295.1	1.006	0.609	145.2
1.75	345.24	3188	4855.0	12.802	1.1447	1.9085	819	0.00112	1.000	294.1	1.000	0.659	157.0
2.00	300.00	3140	4786.1	12.834	1.1456	1.8496	813	0.00106	1.125	295.9	1.014	0.734	175.1
4.00	150.00	2903	4463.7	12.978	1.1526	1.5556	779	0.00136	1.623	322.1	1.339	1.016	242.3
10.00	60.00	2584	4080.8	13.115	1.1702	1.2090	730	0.00102	2.148	359.5	2.356	1.273	303.3
20.00	30.00	2337	3823.0	13.174	1.1884	1.0195	688	0.00073	2.506	383.6	3.803	1.419	338.3
40.00	15.00	2088	3592.0	13.203	1.2067	0.9006	640	0.00070	2.855	404.1	6.256	1.539	366.8
40.83	14.70	2081	3585.6	13.203	1.2072	0.8980	638	0.00070	2.866	404.6	6.350	1.542	367.6
100.00	6.00	1775	3326.0	13.214	1.2263	0.8183	571	0.00077	3.327	426.4	12.271	1.646	397.1
200.00	3.00	1558	3152.5	13.216	1.2387	0.7809	515	0.00070	3.708	440.2	20.571	1.744	415.7
400.00	1.50	1359	3000.6	13.216	1.2515	0.7484	459	0.00063	4.089	451.9	34.597	1.809	431.3
1000.00	0.60	1125	2829.9	13.216	1.2696	0.7080	387	0.00055	4.637	464.6	68.879	1.880	448.2
2000.00	0.30	968	2721.0	13.216	1.2840	0.6798	334	0.00049	5.087	472.4	115.835	1.924	458.6
4000.00	0.15	828	2627.5	13.216	1.2978	0.6552	286	0.00044	5.575	479.0	194.445	1.961	467.4
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	600.00	3481	4586.9	13.859	1.1337	2.4909	875	0.00214	0.000	515.6	2.126	0.000	0.0
1.05	571.43	3465	4562.6	13.875	1.1335	2.4777	873	0.00212	0.294	515.6	2.126	0.198	46.0
1.20	500.00	3422	4496.8	13.919	1.1331	2.4401	867	0.00207	0.570	328.6	1.242	0.381	88.5
1.40	428.57	3373	4422.2	13.969	1.1327	2.3938	861	0.00201	0.778	294.1	1.052	0.516	119.7
1.60	375.00	3331	4358.6	14.012	1.1324	2.3513	855	0.00196	0.924	286.7	1.006	0.607	140.9
1.75	346.81	3306	4321.9	14.037	1.1323	2.3254	851	0.00193	1.000	286.0	1.000	0.654	151.8
2.00	300.00	3261	4254.6	14.082	1.1321	2.2752	845	0.00187	1.129	287.8	1.015	0.733	170.8
4.00	150.00	3052	3948.2	14.288	1.1330	2.0021	816	0.00177	1.630	314.1	1.350	1.016	235.7
10.00	60.00	2779	3579.7	14.522	1.1403	1.5823	775	0.00146	2.155	351.9	2.409	1.276	296.0
20.00	30.00	2568	3327.2	14.656	1.1527	1.2725	741	0.00117	2.505	376.8	3.944	1.427	331.1
40.00	15.00	2346	3097.0	14.745	1.1712	1.0267	703	0.00084	2.837	398.3	6.587	1.552	360.1
40.83	14.70	2340	3090.5	14.747	1.1718	1.0207	702	0.00083	2.846	398.8	6.689	1.555	360.8
100.00	6.00	2042	2826.6	14.800	1.1976	0.8369	642	0.00055	3.275	421.8	13.134	1.687	391.4
200.00	3.00	1815	2647.3	14.812	1.2135	0.7683	591	0.00050	3.623	436.6	22.291	1.771	410.8
400.00	1.50	1602	2488.5	14.815	1.2260	0.7287	537	0.00048	3.991	449.2	37.727	1.842	427.3
1000.00	0.60	1347	2307.6	14.816	1.2422	0.6880	464	0.00040	4.507	463.0	76.063	1.919	445.3
2000.00	0.30	1173	2190.6	14.816	1.2553	0.6594	409	0.00034	4.926	471.6	129.237	1.968	456.6
4000.00	0.15	1016	2089.0	14.816	1.2694	0.6320	356	0.00028	5.375	478.9	219.200	2.009	466.2
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	600.00	3526	4142.9	14.930	1.1295	2.6696	896	0.00214	0.000	500.1	2.123	0.000	0.0
1.05	571.43	3511	4120.1	14.948	1.1293	2.6628	894	0.00213	0.294	500.1	2.123	0.198	44.6
1.20	500.00	3469	4058.3	14.999	1.1285	2.6432	888	0.00209	0.571	318.8	1.241	0.381	85.8
1.40	428.57	3422	3988.0	15.057	1.1277	2.6185	881	0.00205	0.780	285.4	1.052	0.515	116.1
1.60	375.00	3382	3928.2	15.107	1.1270	2.5953	876	0.00202	0.926	278.3	1.005	0.607	136.7
1.75	347.52	3360	3894.5	15.136	1.1267	2.5813	873	0.00200	1.000	277.6	1.000	0.653	147.0
2.00	300.00	3317	3830.1	15.190	1.1260	2.5526	866	0.00195	1.132	279.4	1.016	0.732	165.0
4.00	150.00	3122	3540.7	15.441	1.1236	2.3886	839	0.00164	1.633	305.3	1.350	1.016	228.9
10.00	60.00	2881	3190.4	15.751	1.1229	2.0940	803	0.00131	2.161	342.8	2.437	1.278	287.9
20.00	30.00	2705	2947.8	15.961	1.1254	1.8100	775	0.00102	2.512	367.9	4.032	1.431	322.5
40.00	15.00	2528	2723.3	16.145	1.1327	1.4813	746	0.00072	2.838	390.0	6.838	1.531	351.5
40.83	14.70	2523	2716.9	16.150	1.1330	1.4712	745	0.00071	2.848	390.6	6.947	1.563	352.3
100.00	6.00	2279	2453.5	16.318	1.1553	1.0541	701	0.00045	3.246	414.9	13.977	1.702	383.4
200.00	3.00	2072	2270.2	16.384	1.1797	0.8410	659	0.00035	3.555	430.8	24.037	1.791	403.7
400.00	1.50	1857	2105.2	16.408	1.1999	0.7376	610	0.00024	3.886	444.3	41.251	1.869	421.1
1000.00	0.60	1585	1914.5	16.415	1.2177	0.6704	540	0.00015	4.367	459.3	84.153	1.954	440.3
2000.00	0.30	1397	1789.5	16.416	1.2295	0.6487	486	0.					

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR
LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute;
equilibrium composition during isentropic expansion

Pressure ratio, P_c/P_e	Static pressure, P_c , lb./sq. in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number M	Specific impulse in vacuum, I _{vac} , (lb.)sec./lb.	Area ratio, ϵ	Thrust coefficient, C _f	Specific impulse, I, (lb.)sec./lb.
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	600.00	3534	3777.9	15.886	1.1283	2.6053	910	0.00251	0.000	485.3	2.122	0.000	0.0
1.05	571.43	3519	3756.4	15.906	1.1280	2.6007	907	0.00250	0.295	485.3	1.198	0.198	43.3
1.20	500.00	3478	3698.1	15.961	1.1272	2.5874	902	0.00247	0.572	309.4	1.240	0.381	83.3
1.40	428.57	3431	3631.9	16.024	1.1263	2.5703	895	0.00244	0.780	277.0	1.051	0.515	112.7
1.60	375.00	3392	3575.5	16.078	1.1255	2.5542	889	0.00241	0.926	270.2	1.005	0.606	132.7
1.73	347.72	3370	3544.0	16.108	1.1251	2.5445	886	0.00239	1.000	269.4	1.000	0.652	142.7
2.00	300.00	3327	3483.1	16.168	1.1244	2.5243	880	0.00236	1.132	271.3	1.016	0.732	160.1
4.00	150.00	3137	3210.2	16.441	1.1212	2.4094	852	0.00218	1.634	296.5	1.357	1.016	222.3
10.00	60.00	2903	2879.3	16.785	1.1186	2.2079	817	0.00192	2.162	333.1	2.445	1.278	279.6
20.00	30.00	2738	2649.6	17.030	1.1181	2.0216	791	0.00171	2.514	357.7	4.055	1.432	313.3
40.00	15.00	2578	2436.1	17.258	1.1191	1.8120	765	0.00150	2.842	379.5	6.910	1.562	341.7
40.83	14.70	2573	2430.0	17.265	1.1191	1.8056	764	0.00149	2.852	380.1	7.022	1.565	342.5
100.00	6.00	2371	2177.0	17.526	1.1239	1.5117	728	0.00120	3.255	404.6	14.326	1.706	373.2
200.00	3.00	2214	1997.7	17.695	1.1315	1.2810	697	0.00099	3.558	421.1	25.124	1.799	393.6
400.00	1.50	2052	1832.3	17.830	1.1437	1.0654	663	0.00080	3.857	435.6	44.210	1.881	411.4
1000.00	.60	1826	1634.9	17.947	1.1679	.8338	611	0.00059	4.260	452.2	93.124	1.974	431.8
2000.00	.30	1648	1501.7	17.991	1.1894	.7163	564	0.00048	4.585	462.8	162.695	2.034	445.0
4000.00	.15	1470	1382.4	18.009	1.2091	.6444	514	0.00040	4.942	472.0	282.648	2.087	456.5
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	600.00	3374	2626.1	19.463	1.1327	1.6233	930	0.00163	0.000	421.1	1.242	0.000	0.0
1.20	500.00	3315	2563.9	19.540	1.1321	1.5942	921	0.00158	0.571	273.0	1.242	0.381	73.5
1.40	428.57	3267	2512.4	19.604	1.1317	1.5682	913	0.00155	0.779	244.3	1.052	0.516	99.4
1.60	375.00	3226	2468.5	19.658	1.1314	1.5447	906	0.00151	0.924	238.3	1.006	0.607	117.1
1.73	346.93	3202	2443.3	19.690	1.1313	1.5306	903	0.00150	1.000	237.6	1.000	0.654	126.1
2.00	300.00	3158	2396.7	19.748	1.1310	1.5034	896	0.00146	1.130	239.1	1.015	0.733	141.3
4.00	150.00	2953	2185.1	20.011	1.1313	1.3606	862	0.00128	1.631	261.0	1.351	1.016	195.9
10.00	60.00	2692	1930.2	20.314	1.1356	1.1474	818	0.00104	2.157	292.6	2.415	1.276	246.1
20.00	30.00	2496	1755.2	20.499	1.1432	.9816	782	0.00086	2.509	313.5	3.967	1.428	275.3
40.00	15.00	2297	1594.7	20.640	1.1557	.8274	743	0.00070	2.841	331.7	6.664	1.554	299.6
40.83	14.70	2291	1590.2	20.643	1.1562	.8232	742	0.00070	2.850	332.2	6.768	1.557	300.2
100.00	6.00	2026	1404.5	20.752	1.1791	.6682	685	0.00054	3.268	351.9	13.428	1.691	326.0
200.00	3.00	1818	1277.1	20.792	1.1984	.5904	635	0.00045	3.599	364.7	22.891	1.777	342.6
400.00	1.50	1616	1163.4	20.807	1.2152	.5432	582	0.00039	3.950	375.6	39.039	1.850	356.7
1000.00	.60	1366	1033.2	20.812	1.2336	.5048	509	0.00032	4.450	387.5	79.054	1.931	372.3
2000.00	.30	1195	948.5	20.813	1.2462	.4834	454	0.00027	4.858	395.0	134.733	1.982	382.1
4000.00	.15	1039	874.7	20.813	1.2594	.4636	401	0.00023	5.296	401.4	229.310	2.025	390.4
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	600.00	3158	2016.0	21.832	1.1414	1.1081	919	0.00112	0.000	391.2	2.132	0.000	0.0
1.05	571.43	3141	2002.0	21.850	1.1414	1.1005	917	0.00111	0.293	391.2	1.199	0.199	34.9
1.20	500.00	3097	1964.2	21.900	1.1417	1.0794	909	0.00108	0.568	249.2	1.245	0.383	67.1
1.40	428.57	3046	1921.3	21.956	1.1421	1.0543	900	0.00105	0.776	222.9	1.054	0.517	90.8
1.60	375.00	3002	1884.8	22.003	1.1426	1.0320	893	0.00102	0.920	217.2	1.006	0.609	106.9
1.73	345.45	2975	1862.7	22.031	1.1430	1.0182	888	0.00100	1.000	216.6	1.000	0.658	115.5
2.00	300.00	2929	1825.1	22.078	1.1437	.9940	880	0.00097	1.125	217.9	1.014	0.734	128.9
4.00	150.00	2706	1650.2	22.286	1.1496	.8720	840	0.00083	1.624	237.3	1.341	1.016	178.4
10.00	60.00	2413	1442.0	22.490	1.1641	.7166	784	0.00065	2.151	265.0	2.365	1.273	223.5
20.00	30.00	2189	1301.4	22.588	1.1804	.6182	737	0.00054	2.507	283.0	3.829	1.421	249.4
40.00	15.00	1965	1174.9	22.642	1.1988	.5459	686	0.00045	2.852	298.3	6.321	1.541	270.5
40.83	14.70	1959	1171.4	22.643	1.1994	.5441	684	0.00045	2.863	298.7	6.416	1.544	271.1
100.00	6.00	1678	1028.7	22.670	1.2212	.4875	614	0.00037	3.316	314.9	12.437	1.670	293.1
200.00	3.00	1475	932.9	22.676	1.2351	.4613	557	0.00032	3.683	325.3	20.879	1.749	307.0
400.00	1.50	1289	849.1	22.677	1.2476	.4417	501	0.00028	4.069	334.1	35.155	1.815	318.7
1000.00	.60	1070	754.5	22.677	1.2641	.4194	430	0.00023	4.614	343.6	70.143	1.887	331.3
2000.00	.30	923	694.1	22.677	1.2770	.4040	378	0.00019	5.059	349.5	118.235	1.932	339.2
4000.00	.15	792	642.1	22.677	1.2904	.3894	329	0.00016	5.539	354.5	199.011	1.970	345.8
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	600.00	2747	1381.4	24.718	1.1694	0.6509	869	0.00065	0.000	342.7	2.152	0.000	0.0
1.05	571.43	2729	1370.7	24.729	1.1701	.6451	866	0.00065	0.289	342.7	1.199	0.199	30.6
1.20	500.00	2679	1341.7	24.759	1.1723	.6293	856	0.00062	0.561	217.9	1.254	0.386	58.8
1.40	428.57	2622	1308.9	24.790	1.1749	.6114	845	0.00060	0.766	194.6	1.058	0.522	79.4
1.60	375.00	2573	1281.1	24.815	1.1774	.5963	835	0.00058	0.909	189.4	1.008	0.613	93.4
1.73	346.99	2538	1261.7	24.832	1.1793	.5868	828	0.00057	1.000	188.6	1.000	0.670	102.1
2.00	300.00	2491	1235.9	24.852	1.1819	.5720	819	0.00055	1.112	189.5	1.011	0.739	112.5
4.00	150.00	2237	1105.1	24.937	1.1963	.5039	765	0.00046	1.608	205.1	1.314	1.018	155.0
10.00	60.00	1913	953.9	24.990	1.2209	.4460	690	0.00038	2.146	227.2	2.253	1.266	192.9
20.00	30.00	1682	854.9	25.003	1.2338	.4185	631	0.00033	2.524	241.2	3.569	1.405	214.0
40.00	15.00	1470	768.2	25.007	1.2483	.4000	572	0.00029	2.900	253.0	5.778	1.517	231.0
40.83	14.70	1464	765.6	25.007	1.2487	.3995	571	0.00028	2.911	253.3	5.862	1.520	231.4
100.00	6.00	1220	670.5	25.008	1.2635	.3811	498	0.00024	3.408	265.7	11.130	1.633	248.7
200.00	3.00	1053	608.0	25.008	1.2755	.3679	444	0.00021	3.807	273.4	18.422	1.703	259.4
400.00	1.50	904	554.2	25.008	1.2879	.3555	392	0.00018	4.229	279.9	30.593	1.761	268.3
1000.00	.60	733	494.8	25.008	1.3053	.3398	329	0.00014	4.829	286.9	59.908	1.824	277.8
2000.00	.30	622	457.5	25.008	1.3185	.3290	285	0.00012	5.326	291.1	99.545	1.862	283.5
4000.00	.15	525	426.0	25.008	1.3312	.3194	245	0.00010	5.868	294.6	165.173	1.893	286.3

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute; equilibrium composition during isentropic expansion

Pressure ratio, P_c/P_e	Static pressure, P, lb./sq.in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb)(sec)/lb	Area ratio, A_e	Thrust coefficient, C_F	Specific impulse, I, (lb)(sec)/lb
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	600.00	2381	1054.4	26.323	1.2036	0.4697	806	0.00045	0.000	308.9	2.174	0.000	0.0
1.05	571.43	2362	1045.7	26.328	1.2048	.4663	802	.00045	.285	308.9	2.174	.203	27.6
1.20	500.00	2309	1022.1	26.340	1.2079	.4572	790	.00044	.554	196.0	1.263	.390	53.0
1.40	428.57	2249	995.6	26.352	1.2116	.4473	777	.00042	.756	174.7	1.063	.526	71.5
1.60	375.00	2198	973.2	26.361	1.2149	.4393	765	.00041	.898	169.8	1.010	.618	84.0
1.78	336.49	2157	955.5	26.367	1.2175	.4332	756	.00040	1.000	169.0	1.000	.683	92.8
2.00	300.00	2113	937.0	26.374	1.2202	.4272	746	.00039	1.099	169.6	1.009	.744	101.1
4.00	150.00	1860	833.4	26.396	1.2355	.3982	685	.00034	1.599	182.6	1.293	1.020	138.7
10.00	60.00	1554	715.9	26.405	1.2521	.3743	605	.00028	2.150	201.3	2.182	1.263	171.6
20.00	30.00	1348	640.3	26.406	1.2632	.3612	546	.00025	2.542	213.1	3.423	1.397	189.8
40.00	15.00	1164	574.8	26.406	1.2741	.3499	491	.00022	2.931	222.9	5.493	1.503	204.3
40.83	14.70	1159	573.1	26.406	1.2744	.3495	489	.00022	2.943	223.2	5.572	1.506	204.7
100.00	6.00	952	502.1	26.406	1.2895	.3352	421	.00018	3.458	233.4	10.461	1.613	219.2
200.00	3.00	813	456.1	26.406	1.3022	.3243	371	.00016	3.876	239.8	17.162	1.679	228.2
400.00	1.50	690	417.0	26.406	1.3153	.3139	325	.00013	4.320	245.1	28.237	1.733	235.5
1000.00	.60	551	374.4	26.406	1.3331	.3012	269	.00011	4.959	250.7	54.608	1.790	243.3
2000.00	.30	463	348.0	26.406	1.3460	.2927	232	.00009	5.492	254.0	89.893	1.824	247.9
4000.00	.15	386	325.9	26.406	1.3564	.2864	197	.00007	6.079	256.8	147.835	1.853	251.8
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	600.00	2072	855.0	27.317	1.2317	0.3924	742	0.00136	0.000	282.7	2.190	0.000	0.0
1.05	571.43	2053	847.7	27.319	1.2327	.3908	738	.00036	.282	282.7	2.190	.204	25.2
1.20	500.00	2002	828.0	27.323	1.2355	.3859	725	.00035	.548	179.1	1.270	.393	48.5
1.40	428.57	1944	805.9	27.326	1.2387	.3808	711	.00034	.749	159.4	1.067	.530	65.4
1.60	375.00	1894	787.2	27.329	1.2413	.3767	699	.00033	.890	154.8	1.011	.622	76.8
1.80	333.54	1852	771.3	27.331	1.2436	.3734	689	.00032	1.000	154.0	1.000	.691	85.3
2.00	300.00	1813	757.2	27.332	1.2455	.3706	679	.00031	1.092	154.4	1.007	.747	92.3
4.00	150.00	1578	671.8	27.337	1.2571	.3559	617	.00028	1.594	165.8	1.281	1.023	126.2
10.00	60.00	1303	576.1	27.339	1.2710	.3410	539	.00023	2.152	182.2	2.143	1.262	155.8
20.00	30.00	1122	515.1	27.339	1.2815	.3309	484	.00020	2.551	192.6	3.341	1.393	172.0
40.00	15.00	961	462.7	27.339	1.2929	.3209	432	.00018	2.948	201.2	5.329	1.497	184.7
40.83	14.70	956	461.3	27.339	1.2932	.3206	430	.00018	2.959	201.4	5.405	1.499	185.1
100.00	6.00	777	405.0	27.339	1.3095	.3076	367	.00015	3.488	210.3	10.063	1.603	197.9
200.00	3.00	658	368.9	27.339	1.3228	.2979	321	.00012	3.919	215.8	16.296	1.666	205.7
400.00	1.50	554	338.4	27.339	1.3364	.2887	279	.00011	4.380	220.3	26.787	1.717	212.0
1000.00	.60	438	305.5	27.339	1.3536	.2782	229	.00008	5.049	225.0	51.327	1.771	218.7
2000.00	.30	365	285.3	27.339	1.3633	.2728	195	.00007	5.614	227.8	83.959	1.803	222.6
4000.00	.15	303	268.6	27.339	1.3697	.2693	164	.00006	6.236	230.1	137.411	1.830	225.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Combustion-chamber pressure, 60 pounds per square inch absolute, frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/sq in. abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse, I _{vac} , (lb)(sec)/lb	Area ratio, ϵ	Thrust coefficient, C _F	Specific impulse, I (lb)(sec)/lb
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	60.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000	530.0	2.250	0.000	0.0
1.05	57.14	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	0.271	530.0	2.250	0.210	47.4
1.20	50.00	1129	5218.5	4.416	1.3436	1.7597	303	0.00070	0.527	534.2	1.297	0.403	90.8
1.40	42.86	1085	5141.8	4.416	1.3469	1.7472	293	0.00068	0.722	526.1	1.081	0.543	122.2
1.60	37.50	1049	5077.7	4.416	1.3497	1.7369	285	0.00066	0.860	526.6	1.018	0.636	143.2
1.87	32.17	1008	5006.8	4.416	1.3528	1.7257	276	0.00063	1.000	524.1	1.000	0.725	163.4
2.00	30.00	989	4975.4	4.416	1.3540	1.7210	272	0.00062	1.059	524.4	1.003	0.761	171.5
4.00	15.00	824	4693.4	4.416	1.3651	1.6825	234	0.00052	1.566	501.7	1.233	1.031	232.3
4.08	14.70	819	4685.8	4.416	1.3654	1.6815	232	0.00052	1.579	502.3	1.244	1.038	233.7
10.00	6.00	643	4392.5	4.416	1.3748	1.6505	188	0.00042	2.152	527.5	1.974	1.257	283.1
20.00	3.00	532	4209.8	4.416	1.3799	1.6344	159	0.00035	2.586	543.5	2.982	1.376	309.9
40.00	1.50	439	4058.9	4.416	1.3824	1.6268	133	0.00029	3.031	556.4	4.620	1.467	330.4
100.00	.60	340	3899.0	4.416	1.3882	1.6093	104	0.00023	3.648	569.8	8.432	1.558	350.8
200.00	.30	280	3802.6	4.416	1.3926	1.5961	85	0.00018	4.149	577.7	13.431	1.610	362.6
400.00	.15	230	3723.2	4.416	1.4068	1.5562	70	0.00015	4.675	584.1	21.488	1.652	372.0
1000.00	.06	175	3640.1	4.416	1.4349	1.4847	55	0.00011	5.438	590.6	39.928	1.694	381.6
2000.00	.03	142	3590.9	4.416	1.4550	1.4389	45	0.00009	6.096	594.3	63.572	1.719	387.2
4000.00	.02	114	3551.2	4.416	1.4705	1.4065	36	0.00007	6.845	597.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	60.00	1514	2969.7	5.216	1.3079	1.6183	402	0.00084	0.000	552.1	2.233	0.000	0.0
1.05	57.14	1497	2941.7	5.216	1.3090	1.6140	399	0.00083	0.274	552.1	2.233	0.209	49.3
1.20	50.00	1450	2866.8	5.216	1.3120	1.6022	389	0.00081	0.533	548.6	1.289	0.400	94.6
1.40	42.86	1398	2783.2	5.216	1.3155	1.5887	378	0.00078	0.730	509.3	1.077	0.539	127.4
1.60	37.50	1354	2713.2	5.216	1.3185	1.5772	369	0.00076	0.869	509.6	1.016	0.632	149.4
1.85	32.49	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	507.3	1.000	0.716	169.2
2.00	30.00	1282	2601.2	5.216	1.3236	1.5584	353	0.00072	1.068	507.8	1.004	0.757	179.1
4.00	15.00	1079	2290.0	5.216	1.3391	1.5045	307	0.00061	1.572	516.7	1.244	1.029	243.2
4.08	14.70	1073	2281.6	5.216	1.3395	1.5031	306	0.00061	1.585	517.4	1.256	1.035	244.7
10.00	6.00	852	1954.3	5.216	1.3559	1.4516	251	0.00048	2.148	544.7	2.009	1.257	297.2
20.00	3.00	709	1748.8	5.216	1.3656	1.4232	213	0.00040	2.573	562.0	3.049	1.379	325.9
40.00	1.50	588	1578.0	5.216	1.3715	1.4066	179	0.00034	3.010	576.0	4.739	1.472	348.0
100.00	.60	458	1396.4	5.216	1.3771	1.3913	142	0.00026	3.619	590.5	8.679	1.565	370.0
200.00	.30	379	1286.2	5.216	1.3811	1.3807	117	0.00022	4.111	599.1	13.870	1.619	382.7
400.00	.15	312	1195.2	5.216	1.3861	1.3677	96	0.00018	4.638	606.1	22.295	1.662	392.9
1000.00	.06	242	1099.3	5.216	1.3973	1.3400	74	0.00013	5.394	613.4	41.978	1.706	403.5
2000.00	.03	198	1041.2	5.216	1.4156	1.2977	61	0.00011	6.014	617.6	67.687	1.733	409.6
4000.00	.02	161	994.0	5.216	1.4350	1.2568	50	0.00009	6.704	621.1	108.753	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	60.00	1816	1249.3	6.015	1.2835	1.4954	481	0.00092	0.000	563.4	2.219	0.000	0.0
1.05	57.14	1797	1220.2	6.015	1.2845	1.4916	477	0.00091	0.276	563.4	2.219	0.207	50.3
1.20	50.00	1744	1142.1	6.015	1.2871	1.4812	467	0.00088	0.538	556.1	1.283	0.398	96.6
1.40	42.86	1685	1054.8	6.015	1.2901	1.4692	456	0.00086	0.736	516.2	1.073	0.536	130.1
1.60	37.50	1635	981.6	6.015	1.2927	1.4590	446	0.00083	0.876	506.6	1.015	0.629	154.6
1.83	32.78	1586	910.0	6.015	1.2955	1.4484	436	0.00081	1.000	504.5	1.000	0.708	171.8
2.00	30.00	1554	864.1	6.015	1.2973	1.4414	429	0.00080	1.076	505.1	1.005	0.754	183.1
4.00	15.00	1322	535.4	6.015	1.3126	1.3872	378	0.00068	1.578	525.4	1.256	1.027	249.2
4.08	14.70	1315	526.5	6.015	1.3130	1.3857	376	0.00068	1.592	526.1	1.267	1.033	250.8
10.00	6.00	1057	176.7	6.015	1.3330	1.3224	314	0.00054	2.147	555.2	2.048	1.258	305.5
20.00	3.00	886	9954.7	6.015	1.3461	1.2847	269	0.00046	2.563	573.6	3.127	1.382	335.6
40.00	1.50	740	9768.9	6.015	1.3569	1.2558	228	0.00038	2.987	588.5	4.883	1.478	358.9
100.00	.60	580	9570.0	6.015	1.3664	1.2320	181	0.00030	3.581	604.1	8.984	1.575	382.3
200.00	.30	481	9448.9	6.015	1.3717	1.2191	151	0.00025	4.064	613.3	14.394	1.650	395.8
400.00	.15	399	9348.4	6.015	1.3755	1.2100	124	0.00020	4.582	620.8	23.204	1.675	406.7
1000.00	.06	310	9241.7	6.015	1.3821	1.1948	95	0.00015	5.328	628.6	43.886	1.722	418.0
2000.00	.03	256	9177.2	6.015	1.3886	1.1805	78	0.00012	5.945	633.3	71.266	1.749	424.6
4000.00	.02	210	9124.0	6.015	1.4039	1.1482	64	0.00010	6.607	637.0	115.624	1.771	430.0
R = 0.300, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	60.00	2089	9932.7	6.812	1.2649	1.3928	550	0.00097	0.000	568.1	2.208	0.000	0.0
1.05	57.14	2068	9903.2	6.812	1.2657	1.3898	546	0.00096	0.278	568.1	2.208	0.206	50.7
1.20	50.00	2011	9232.7	6.812	1.2678	1.3811	536	0.00094	0.541	559.4	1.278	0.396	97.4
1.40	42.86	1946	9734.8	6.812	1.2704	1.3707	524	0.00091	0.741	519.4	1.071	0.533	131.3
1.60	37.50	1891	9660.0	6.812	1.2727	1.3616	514	0.00089	0.881	509.9	1.013	0.626	154.0
1.82	33.01	1840	9590.5	6.812	1.2730	1.3527	504	0.00087	1.000	507.9	1.000	0.701	172.6
2.00	30.00	1803	9539.8	6.812	1.2767	1.3460	497	0.00085	1.082	508.6	1.008	0.752	186.9
4.00	15.00	1547	9201.7	6.812	1.2901	1.2972	463	0.00074	1.585	530.1	1.245	1.023	252.2
4.08	14.70	1540	9192.5	6.812	1.2906	1.2958	442	0.00073	1.598	530.8	1.278	1.032	253.8
10.00	6.00	1252	8828.7	6.812	1.3101	1.2326	374	0.00060	2.148	561.2	2.084	1.260	310.0
20.00	3.00	1059	8595.4	6.812	1.3254	1.1882	324	0.00050	2.555	580.5	3.204	1.386	341.1
40.00	1.50	891	8398.5	6.812	1.3389	1.1523	277	0.00042	2.969	596.3	5.032	1.485	365.4
100.00	.60	704	8186.3	6.812	1.3535	1.1170	224	0.00033	3.545	612.7	9.315	1.584	389.8
200.00	.30	587	8056.1	6.812	1.3607	1.1005	186	0.00027	4.015	622.5	14.975	1.642	404.1
400.00	.15	487	7947.8	6.812	1.3669	1.0868	155	0.00023	4.519	630.5	24.203	1.689	415.6
1000.00	.06	381	7832.4	6.812	1.3727	1.0745	119	0.00017	5.249	638.8	45.935	1.738	427.5
2000.00	.03	315	7762.2	6.812	1.3777	1.0640	97	0.00014	5.855	643.8	74.800	1.766	434.6
4000.00	.02	260	7704.2	6.812	1.3833	1.0529	79	0.00011	6.513	647.9	121.990	1.790	440.4

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN
 [Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P, lb/sq in abs	Temperature, T, K	Enthalpy, h, cal/s	Molecular weight, M	Isentropic exponent, γ	Specific heat, C_p , cal/(g)(K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(K)(cm)	Mach number M	Specific impulse in vacuum, I_{vac} , (lb)(sec)/lb	Area ratio, E	Thrust coefficient, C_f	Specific impulse, I , (lb)(sec)/(lb)
R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	60.00	2329	8892.8	7.597	1.2510	1.3038	608	0.00099	0.000	568.1	2.199	0.000	0.0
1.05	57.14	2307	8863.2	7.597	1.2516	1.3011	604	0.00098	0.280	569.7	2.199	0.205	50.7
1.20	50.00	2245	8783.7	7.597	1.2534	1.2936	594	0.00096	0.544	570.7	1.274	0.394	97.4
1.40	42.86	2176	8694.6	7.597	1.2556	1.2849	582	0.00094	0.745	571.9	1.069	0.532	131.3
1.60	37.50	2118	8619.6	7.597	1.2575	1.2774	572	0.00092	0.886	572.5	1.012	0.624	154.2
1.80	33.18	2065	8552.7	7.597	1.2593	1.2705	563	0.00090	1.000	573.6	1.000	0.696	172.0
2.00	30.00	2023	8498.8	7.597	1.2608	1.2646	555	0.00088	1.087	574.5	1.006	0.750	185.2
4.00	15.00	1748	8157.4	7.597	1.2726	1.2411	501	0.00078	1.590	581.6	1.273	1.024	253.0
4.08	14.70	1741	8148.1	7.597	1.2730	1.2419	499	0.00077	1.603	582.4	1.286	1.030	256.6
10.00	6.00	1430	7777.6	7.597	1.2906	1.1616	429	0.00064	2.150	593.7	2.114	1.261	311.5
20.00	3.00	1219	7537.8	7.597	1.3057	1.1171	376	0.00054	2.951	593.8	3.272	1.390	343.4
40.00	1.50	1033	7334.0	7.597	1.3209	1.0765	325	0.00046	2.955	600.2	5.170	1.491	368.3
100.00	.60	823	7112.3	7.597	1.3363	1.0347	263	0.00036	3.515	617.4	9.636	1.593	393.6
200.00	.30	689	6975.5	7.597	1.3540	1.0110	221	0.00030	3.970	627.7	15.552	1.653	408.4
400.00	.15	575	6861.1	7.597	1.3568	.9946	185	0.00024	4.461	636.0	23.218	1.702	420.5
1000.00	.06	451	6738.6	7.597	1.3645	.9790	145	0.00019	5.172	644.8	48.013	1.753	432.9
2000.00	.03	375	6664.0	7.597	1.3696	.9692	118	0.00015	5.763	650.1	78.373	1.783	440.4
4000.00	.02	310	6602.0	7.597	1.3746	.9598	96	0.00012	6.407	654.4	128.116	1.807	446.5
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	60.00	2531	8050.5	8.363	1.2404	1.2259	656	0.00100	0.000	564.6	2.193	0.000	0.0
1.05	57.14	2508	8021.3	8.363	1.2410	1.2237	653	0.00099	0.281	566.6	2.193	0.205	50.4
1.20	50.00	2443	7942.8	8.363	1.2425	1.2174	642	0.00097	0.547	567.7	1.271	0.393	96.8
1.40	42.86	2371	7854.5	8.363	1.2444	1.2099	631	0.00095	0.748	568.3	1.067	0.530	130.6
1.60	37.50	2309	7766.4	8.363	1.2461	1.2033	620	0.00093	0.889	569.0	1.012	0.623	153.3
1.80	33.18	2256	7716.2	8.363	1.2476	1.1972	611	0.00091	1.000	569.3	1.000	0.693	170.6
2.00	30.00	2209	7660.6	8.363	1.2490	1.1919	603	0.00090	1.091	569.2	1.007	0.748	184.2
4.00	15.00	1920	7321.0	8.363	1.2591	1.1547	549	0.00080	1.594	580.7	1.280	1.023	251.9
4.08	14.70	1912	7311.7	8.363	1.2594	1.1536	548	0.00079	1.607	581.5	1.292	1.030	255.5
10.00	6.00	1583	6940.6	8.363	1.2752	1.1009	476	0.00067	2.151	593.4	2.138	1.262	310.8
20.00	3.00	1359	6698.7	8.363	1.2894	1.0585	421	0.00057	2.948	593.9	3.327	1.393	343.0
40.00	1.50	1159	6491.7	8.363	1.3046	1.0178	368	0.00048	2.945	600.8	5.287	1.496	368.3
100.00	.60	931	6264.8	8.363	1.3239	.9712	301	0.00038	3.492	618.6	9.918	1.601	394.2
200.00	.30	784	6123.9	8.363	1.3366	.9436	255	0.00032	3.934	629.2	16.077	1.663	409.4
400.00	.15	657	6005.5	8.363	1.3467	.9230	214	0.00026	4.411	637.9	26.157	1.713	421.8
1000.00	.06	518	5878.1	8.363	1.3573	.9026	168	0.00020	5.102	647.1	49.977	1.766	434.8
2000.00	.03	431	5800.3	8.363	1.3627	.8928	139	0.00016	5.680	652.6	81.743	1.797	442.5
4000.00	.02	358	5735.5	8.363	1.3660	.8833	113	0.00013	6.309	657.1	133.696	1.823	448.8
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	60.00	2696	7354.5	9.102	1.2326	1.1570	696	0.00099	0.000	558.6	2.188	0.000	0.0
1.05	57.14	2671	7325.9	9.102	1.2331	1.1550	692	0.00099	0.282	558.6	2.188	0.205	49.9
1.20	50.00	2604	7249.0	9.102	1.2344	1.1496	682	0.00097	0.548	559.0	1.269	0.392	95.8
1.40	42.86	2529	7162.6	9.102	1.2360	1.1434	670	0.00095	0.750	559.1	1.066	0.529	129.2
1.60	37.50	2465	7089.8	9.102	1.2375	1.1377	660	0.00093	0.891	559.1	1.011	0.622	151.8
1.80	33.18	2411	7028.4	9.102	1.2388	1.1326	651	0.00092	1.000	559.4	1.000	0.690	168.4
2.00	30.00	2362	6972.2	9.102	1.2401	1.1278	643	0.00090	1.093	559.4	1.008	0.747	182.4
4.00	15.00	2061	6638.0	9.102	1.2490	1.0950	589	0.00081	1.597	572.1	1.284	1.023	249.7
4.08	14.70	2053	6628.8	9.102	1.2493	1.0940	587	0.00080	1.610	572.9	1.297	1.029	251.3
10.00	6.00	1710	6261.7	9.102	1.2637	1.0464	516	0.00068	2.153	581.0	2.157	1.263	304.4
20.00	3.00	1476	6021.0	9.102	1.2766	1.0076	460	0.00059	2.947	581.8	3.370	1.395	340.6
40.00	1.50	1266	5813.8	9.102	1.2911	.9682	405	0.00050	2.938	590.0	5.380	1.500	366.1
100.00	.60	1024	5585.4	9.102	1.3112	.9199	334	0.00040	3.474	617.1	10.154	1.607	392.3
200.00	.30	866	5442.7	9.102	1.3250	.8901	285	0.00033	3.906	628.0	16.525	1.670	407.9
400.00	.15	729	5322.2	9.102	1.3373	.8657	241	0.00027	4.370	637.0	26.977	1.722	420.5
1000.00	.06	577	5192.1	9.102	1.3495	.8430	190	0.00021	5.045	646.4	51.722	1.777	433.8
2000.00	.03	481	5112.3	9.102	1.3569	.8300	158	0.00017	5.609	652.0	84.764	1.809	441.7
4000.00	.02	401	5045.7	9.102	1.3625	.8207	129	0.00014	6.225	656.7	139.079	1.836	448.2
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	60.00	2828	6769.6	9.811	1.2265	1.0967	728	0.00098	0.000	551.1	2.184	0.000	0.0
1.05	57.14	2802	6741.8	9.811	1.2270	1.0949	724	0.00098	0.283	551.1	2.184	0.204	49.2
1.20	50.00	2734	6666.9	9.811	1.2283	1.0899	714	0.00096	0.550	551.1	1.268	0.392	94.5
1.40	42.86	2657	6582.8	9.811	1.2298	1.0841	702	0.00094	0.751	551.1	1.065	0.528	127.5
1.60	37.50	2591	6511.8	9.811	1.2311	1.0791	692	0.00092	0.893	551.1	1.011	0.621	149.8
1.79	33.49	2536	6453.1	9.811	1.2322	1.0749	684	0.00091	1.000	551.1	1.000	0.688	166.0
2.00	30.00	2484	6397.2	9.811	1.2335	1.0706	675	0.00089	1.096	551.1	1.008	0.746	180.0
4.00	15.00	2175	6070.5	9.811	1.2415	1.0411	622	0.00080	1.599	574.4	1.288	1.022	246.6
4.08	14.70	2166	6061.5	9.811	1.2418	1.0402	620	0.00080	1.612	575.1	1.301	1.029	248.2
10.00	6.00	1813	5701.2	9.811	1.2548	.9976	549	0.00069	2.153	587.3	2.172	1.264	304.9
20.00	3.00	1571	5463.9	9.811	1.2687	.9619	492	0.00060	2.945	587.1	3.406	1.397	337.1
40.00	1.50	1354	5258.9	9.811	1.2866	.9245	436	0.00051	2.933	595.5	5.454	1.503	362.6
100.00	.60	1102	5031.6	9.811	1.3005	.8769	363	0.00041	3.461	613.8	10.345	1.612	388.9
200.00	.30	936	4888.8	9.811	1.3150	.8455	312	0.00034	3.885	624.9	18.895	1.677	404.5
400.00	.15	790	4767.9	9.811	1.3283	.8194	264	0.00028	4.339	634.0	27.668	1.730	417.3
1000.00	.06	628	4636.8	9.811	1.3426	.7938	209	0.00022	4.999	643.6	53.222	1.785	430.8
2000.00	.03	525	4556.1	9.811	1.3514	.7790	173	0.00018	5.550	649.4	87.397	1.819	438.9
4000.00	.02	438	4488.6	9.811	1.3579	.7685	143	0.00015	6.154	654.2	143.606	1.846	445.5

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; Frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P ₀ , lb/in ² abs	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g ^{1/2} K ^{1/2})	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec ^{1/2} K ^{1/2} cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb)(sec ^{1/2})/lb	Area ratio, ϵ	Thrust coefficient, C _F	Specific impulse, I _s , (lb)(sec ^{1/2})/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	60.00	3015	5841.6	11.142	1.2182	0.9956	777	0.00095	0.000	0.000	2.179	0.000	0.0
1.05	57.14	2989	5615.5	11.142	1.2186	.9942	775	.00094	.284	534.1	2.179	.203	47.7
1.20	50.00	2918	5745.1	11.142	1.2197	.9901	765	.00093	.591	338.8	1.265	.391	91.6
1.40	42.86	2838	5666.0	11.142	1.2210	.9853	751	.00091	.754	301.8	1.084	.527	123.6
1.60	37.50	2770	5599.2	11.142	1.2222	.9810	741	.00089	.896	293.2	1.010	.620	145.2
1.78	33.59	2715	5545.4	11.142	1.2232	.9774	733	.00088	1.000	291.8	1.000	.685	160.5
2.00	30.00	2660	5491.2	11.142	1.2242	.9737	724	.00087	1.099	292.8	1.008	.745	174.6
4.00	15.00	2339	5182.6	11.142	1.2312	.9498	671	.00079	1.602	315.3	1.293	1.022	239.5
4.08	14.70	2330	5176.1	11.142	1.2314	.9491	669	.00078	1.615	316.0	1.297	1.028	241.0
10.00	6.00	1963	4831.8	11.142	1.2426	.9136	598	.00068	2.155	347.8	2.192	1.265	296.4
20.00	3.00	1710	4605.0	11.142	1.2533	.8826	541	.00060	2.543	368.5	3.452	1.399	328.0
40.00	1.50	1483	4407.9	11.142	1.2626	.8499	484	.00052	2.927	385.8	5.559	1.507	353.2
100.00	.60	1217	4187.7	11.142	1.2685	.8057	409	.00042	3.444	404.2	10.821	1.618	379.4
200.00	.30	1041	4046.4	11.142	1.2595	.7739	354	.00035	3.856	415.5	17.444	1.685	395.0
400.00	.15	884	3929.6	11.142	1.3139	.7464	303	.00029	4.295	424.7	28.712	1.740	407.9
1000.00	.06	707	3800.0	11.142	1.3311	.7170	242	.00023	4.931	434.5	55.548	1.798	421.5
2000.00	.03	594	3719.7	11.142	1.3414	.7007	202	.00019	5.465	440.4	91.527	1.833	429.7
4000.00	.02	497	3652.4	11.142	1.3504	.6874	168	.00015	6.048	445.3	150.804	1.862	436.4
R = 0.700, PERCENT FUEL = 16.25, O/F = 5.556													
1.00	60.00	3128	5138.3	12.360	1.2132	0.9147	811	0.00090	0.000	0.000	2.176	0.000	0.0
1.05	57.14	3101	5113.9	12.360	1.2136	.9135	807	.00090	.284	516.6	2.176	.203	46.1
1.20	50.00	3029	5048.1	12.360	1.2146	.9101	797	.00089	.552	327.7	1.264	.390	88.6
1.40	42.86	2947	4974.0	12.360	1.2157	.9060	785	.00087	.755	292.0	1.063	.527	119.6
1.60	37.50	2878	4911.5	12.360	1.2168	.9024	775	.00085	.898	283.8	1.010	.619	140.5
1.78	33.59	2823	4861.9	12.360	1.2177	.8993	766	.00084	1.000	282.4	1.000	.683	155.1
2.00	30.00	2765	4810.3	12.360	1.2187	.8960	758	.00083	1.100	283.4	1.009	.744	168.9
4.00	15.00	2439	4520.6	12.360	1.2249	.8755	704	.00076	1.604	305.4	1.296	1.021	231.8
4.08	14.70	2429	4512.6	12.360	1.2251	.8749	702	.00076	1.617	306.2	1.310	1.028	233.3
10.00	6.00	2055	4190.3	12.360	1.2353	.8440	631	.00066	2.156	337.2	2.204	1.265	287.2
20.00	3.00	1797	3975.9	12.360	1.2451	.8168	574	.00058	2.542	357.5	3.481	1.401	318.0
40.00	1.50	1564	3788.9	12.360	1.2564	.7879	517	.00051	2.923	374.6	5.624	1.509	342.7
100.00	.60	1291	3579.1	12.360	1.2741	.7473	440	.00042	3.434	392.8	10.796	1.623	368.3
200.00	.30	1108	3445.6	12.360	1.2890	.7171	384	.00035	3.839	404.0	17.977	1.691	383.8
400.00	.15	946	3331.4	12.360	1.3040	.6897	331	.00029	4.269	413.2	29.399	1.747	396.5
1000.00	.06	760	3206.1	12.360	1.3224	.6595	265	.00023	4.890	423.0	57.120	1.806	410.0
2000.00	.03	640	3128.2	12.360	1.3341	.6420	223	.00019	5.410	428.9	94.365	1.852	418.2
4000.00	.02	537	3062.8	12.360	1.3441	.6260	186	.00015	5.979	433.8	155.825	1.872	425.0
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	60.00	3188	4586.9	13.470	1.2103	0.8490	835	0.00086	0.000	0.000	2.174	0.000	0.0
1.05	57.14	3161	4564.0	13.470	1.2106	.8480	831	.00086	.285	499.6	2.174	.203	44.6
1.20	50.00	3088	4502.5	13.470	1.2115	.8451	821	.00084	.553	317.0	1.263	.390	85.7
1.40	42.86	3006	4433.2	13.470	1.2126	.8415	809	.00083	.756	282.5	1.063	.526	115.6
1.60	37.50	2936	4374.7	13.470	1.2136	.8382	798	.00082	.899	274.6	1.010	.618	135.9
1.78	33.59	2881	4328.7	13.470	1.2144	.8356	790	.00081	1.000	273.3	1.000	.682	149.9
2.00	30.00	2823	4279.9	13.470	1.2154	.8326	781	.00079	1.101	274.3	1.009	.744	163.4
4.00	15.00	2493	4008.4	13.470	1.2215	.8143	727	.00073	1.605	295.7	1.298	1.021	224.4
4.08	14.70	2484	4000.9	13.470	1.2215	.8137	725	.00072	1.618	296.4	1.312	1.028	225.8
10.00	6.00	2106	3698.1	13.470	1.2311	.7860	654	.00063	2.156	326.7	2.212	1.266	278.1
20.00	3.00	1845	3496.4	13.470	1.2402	.7617	597	.00056	2.542	346.5	3.499	1.402	308.0
40.00	1.50	1609	3319.9	13.470	1.2509	.7355	539	.00050	2.921	363.1	5.664	1.511	332.0
100.00	.60	1333	3121.5	13.470	1.2690	.6980	462	.00041	3.429	381.0	10.902	1.625	357.1
200.00	.30	1148	2994.8	13.470	1.2824	.6699	402	.00035	3.829	392.0	18.014	1.694	372.2
400.00	.15	982	2880.1	13.470	1.2975	.6434	350	.00029	4.254	401.1	29.828	1.751	384.7
1000.00	.06	792	2766.6	13.470	1.3164	.6138	284	.00023	4.865	410.8	58.120	1.811	398.0
2000.00	.03	669	2692.0	13.470	1.3290	.5960	239	.00019	5.377	416.6	98.197	1.848	406.1
4000.00	.02	562	2624.2	13.470	1.3397	.5819	200	.00015	5.937	421.5	159.100	1.878	412.7
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	60.00	3213	4142.9	14.479	1.2086	0.7951	852	0.00082	0.000	0.000	2.173	0.000	0.0
1.05	57.14	3186	4121.5	14.479	1.2089	.7942	848	.00082	.285	483.8	2.173	.203	43.2
1.20	50.00	3113	4063.8	14.479	1.2098	.7915	837	.00081	.553	307.0	1.263	.390	83.0
1.40	42.86	3031	3998.8	14.479	1.2108	.7883	825	.00079	.757	273.6	1.063	.526	112.0
1.60	37.50	2961	3943.9	14.479	1.2118	.7853	815	.00078	.899	266.0	1.010	.618	131.6
1.78	33.72	2907	3901.1	14.479	1.2126	.7829	806	.00077	1.000	264.7	1.000	.681	145.1
2.00	30.00	2848	3854.9	14.479	1.2135	.7802	797	.00076	1.102	265.7	1.009	.744	158.3
4.00	15.00	2518	3600.0	14.479	1.2192	.7634	742	.00069	1.606	286.5	1.299	1.021	217.4
4.08	14.70	2508	3592.9	14.479	1.2194	.7629	741	.00069	1.619	287.2	1.313	1.028	218.8
10.00	6.00	2129	3308.4	14.479	1.2287	.7374	669	.00061	2.156	316.7	2.216	1.266	269.5
20.00	3.00	1868	3118.4	14.479	1.2378	.7153	611	.00054	2.541	335.9	3.509	1.402	298.6
40.00	1.50	1632	2952.2	14.479	1.2470	.6910	553	.00048	2.919	352.2	5.686	1.512	321.9
100.00	.60	1374	2764.9	14.479	1.2644	.6562	476	.00039	3.425	369.6	10.964	1.626	346.3
200.00	.30	1186	2645.1	14.479	1.2786	.6299	418	.00034	3.824	380.3	18.140	1.696	361.0
400.00	.15	1001	2542.1	14.479	1.2936	.6048	363	.00028	4.245	389.2	30.080	1.753	373.2
1000.00	.06	809	2428.7	14.479	1.3100	.5762	295	.00022	4.851	398.7	58.719	1.814	386.2
2000.00	.03	684	2357.8	14.479	1.3230	.5580	250	.00018	5.357	404.5	97.311	1.851	394.1
4000.00	.02	575	2298.1	14.479	1.3357	.5446	210	.00015	5.912	409.2	161.114	1.882	400.7

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/sq in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K) cm	Mach number M	Specific impulse in vacuum, I _{vac} , lb(sec)/lb	Area ratio, A	Thrust coefficient, C _f	Specific impulse, I, lb(sec)/lb
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	60.00	3217	3777.9	15.399	1.2077	0.7503	864	0.0009	0.000	0.000		0.000	0.0
1.05	57.14	3190	3757.7	15.399	1.2080	0.7494	860	0.0008	0.285	469.4	2.173	0.203	41.9
1.20	50.00	3118	3703.4	15.399	1.2088	0.7470	849	0.0007	0.554	297.9	1.262	0.390	86.5
1.40	42.86	3036	3642.1	15.399	1.2099	0.7439	837	0.0006	0.757	265.5	1.063	0.526	108.7
1.60	37.50	2968	3590.4	15.399	1.2108	0.7412	826	0.0005	0.899	258.1	1.010	0.618	127.7
1.78	33.73	2912	3550.2	15.399	1.2116	0.7389	818	0.0004	1.000	256.9	1.000	0.681	140.7
2.00	30.00	2853	3506.7	15.399	1.2125	0.7364	808	0.0003	1.102	257.9	1.009	0.743	153.6
4.00	15.00	2523	3266.5	15.399	1.2181	0.7207	753	0.0006	1.606	278.1	1.300	1.021	210.9
4.08	14.70	2514	3259.8	15.399	1.2185	0.7202	751	0.0006	1.619	278.8	1.313	1.027	212.3
10.00	6.00	2135	2991.6	15.399	1.2274	0.6965	678	0.0008	2.156	307.4	2.218	1.266	261.6
20.00	3.00	1875	2812.4	15.399	1.2360	0.6759	621	0.0002	2.541	326.2	3.515	1.403	289.8
40.00	1.50	1638	2655.5	15.399	1.2462	0.6532	562	0.0006	2.919	341.9	5.698	1.512	312.5
100.00	.60	1361	2478.5	15.399	1.2625	0.6207	485	0.0008	3.424	359.0	10.997	1.627	336.2
200.00	.30	1175	2365.3	15.399	1.2764	0.5960	427	0.0002	3.821	369.4	18.208	1.697	350.6
400.00	.15	1008	2267.8	15.399	1.2912	0.5722	372	0.0007	4.241	378.1	30.218	1.754	362.5
1000.00	.06	815	2160.3	15.399	1.3105	0.5449	304	0.0001	4.844	387.4	59.055	1.816	375.2
2000.00	.03	690	2093.1	15.399	1.3235	0.5280	258	0.0006	5.347	393.0	97.944	1.853	382.9
4000.00	.02	581	2036.3	15.399	1.3348	0.5145	217	0.0005	5.898	397.7	162.275	1.884	389.3
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	60.00	3116	2626.1	18.987	1.2082	0.6073	889	0.0006	0.000	0.000		0.000	0.0
1.05	57.14	3090	2610.2	18.987	1.2085	0.6065	884	0.0005	0.285	416.0	2.173	0.203	37.1
1.20	50.00	3019	2567.5	18.987	1.2094	0.6044	873	0.0004	0.553	264.0	1.262	0.390	71.4
1.40	42.86	2939	2519.5	18.987	1.2105	0.6019	859	0.0003	0.757	235.3	1.063	0.526	96.3
1.60	37.50	2872	2478.9	18.987	1.2115	0.5996	848	0.0002	0.899	228.7	1.010	0.618	113.2
1.78	33.72	2819	2447.2	18.987	1.2125	0.5977	839	0.0001	1.000	227.6	1.000	0.681	124.7
2.00	30.00	2762	2413.1	18.987	1.2132	0.5956	829	0.0000	1.102	228.5	1.009	0.744	136.1
4.00	15.00	2442	2224.5	18.987	1.2189	0.5828	770	0.0005	1.606	246.4	1.300	1.021	186.9
4.08	14.70	2433	2219.3	18.987	1.2191	0.5824	768	0.0005	1.619	247.0	1.313	1.028	188.1
10.00	6.00	2066	2008.8	18.987	1.2282	0.5635	692	0.0008	2.156	272.3	2.217	1.266	231.8
20.00	3.00	1813	1886.3	18.987	1.2368	0.5466	632	0.0003	2.542	288.9	3.511	1.402	256.8
40.00	1.50	1584	1745.2	18.987	1.2467	0.5289	573	0.0008	2.920	302.9	5.691	1.512	276.9
100.00	.60	1315	1606.5	18.987	1.2624	0.5035	495	0.0001	3.425	318.0	10.982	1.627	297.9
200.00	.30	1136	1517.7	18.987	1.2757	0.4843	439	0.0007	3.824	327.2	18.188	1.696	310.6
400.00	.15	975	1441.2	18.987	1.2898	0.4658	384	0.0003	4.244	334.9	30.198	1.754	321.1
1000.00	.06	789	1356.9	18.987	1.3082	0.4442	317	0.0008	4.846	343.1	59.073	1.815	332.3
2000.00	.03	669	1304.1	18.987	1.3212	0.4305	271	0.0005	5.347	348.1	98.060	1.852	339.2
4000.00	.02	564	1259.5	18.987	1.3329	0.4190	230	0.0003	5.896	352.3	162.595	1.883	344.8
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	60.00	2966	2016.0	21.453	1.2116	0.5304	885	0.0007	0.000	0.000		0.000	0.0
1.05	57.14	2941	2002.7	21.453	1.2119	0.5297	882	0.0007	0.284	381.8	2.175	0.203	34.1
1.20	50.00	2873	1966.7	21.453	1.2129	0.5277	870	0.0006	0.553	242.3	1.264	0.390	65.5
1.40	42.86	2796	1926.3	21.453	1.2141	0.5253	856	0.0005	0.756	215.9	1.063	0.526	88.4
1.60	37.50	2731	1892.1	21.453	1.2151	0.5232	844	0.0004	0.898	209.8	1.010	0.619	103.9
1.78	33.58	2679	1865.1	21.453	1.2160	0.5215	834	0.0003	1.000	208.8	1.000	0.683	114.6
2.00	30.00	2625	1836.7	21.453	1.2169	0.5196	824	0.0002	1.101	209.6	1.009	0.744	124.9
4.00	15.00	2316	1678.3	21.453	1.2250	0.5079	763	0.0008	1.606	225.9	1.297	1.021	171.4
4.08	14.70	2308	1673.9	21.453	1.2252	0.5076	761	0.0007	1.618	226.4	1.311	1.028	172.5
10.00	6.00	1954	1497.4	21.453	1.2327	0.4906	689	0.0001	2.156	249.5	2.208	1.265	212.4
20.00	3.00	1711	1379.8	21.453	1.2416	0.4760	622	0.0007	2.543	264.6	3.492	1.401	235.3
40.00	1.50	1492	1277.1	21.453	1.2517	0.4607	562	0.0002	2.923	277.3	5.650	1.510	253.6
100.00	.60	1236	1161.6	21.453	1.2671	0.4394	486	0.0007	3.433	290.9	10.878	1.624	272.7
200.00	.30	1065	1087.9	21.453	1.2801	0.4233	431	0.0003	3.835	299.3	17.986	1.693	284.2
400.00	.15	912	1024.5	21.453	1.2935	0.4082	378	0.0000	4.259	306.2	29.822	1.750	293.7
1000.00	.06	737	954.7	21.453	1.3114	0.3901	313	0.0006	4.868	313.7	58.249	1.810	303.9
2000.00	.03	624	911.1	21.453	1.3241	0.3764	269	0.0003	5.374	318.2	96.601	1.847	310.1
4000.00	.02	525	874.3	21.453	1.3358	0.3665	229	0.0001	5.927	321.9	160.627	1.877	315.2
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	60.00	2655	1381.4	24.532	1.2209	0.4476	851	0.0007	0.000	0.000		0.000	0.0
1.05	57.14	2632	1371.0	24.532	1.2213	0.4470	847	0.0006	0.283	337.8	2.181	0.204	30.1
1.20	50.00	2569	1342.8	24.532	1.2224	0.4452	834	0.0006	0.551	214.2	1.266	0.391	57.9
1.40	42.86	2498	1311.2	24.532	1.2237	0.4430	820	0.0005	0.753	190.8	1.064	0.528	78.2
1.60	37.50	2437	1284.5	24.532	1.2249	0.4411	807	0.0004	0.895	185.4	1.010	0.620	91.8
1.78	33.56	2388	1262.8	24.532	1.2260	0.4395	797	0.0003	1.000	184.4	1.000	0.688	101.6
2.00	30.00	2339	1241.4	24.532	1.2270	0.4378	787	0.0002	1.098	185.1	1.008	0.745	110.4
4.00	15.00	2054	1118.2	24.532	1.2340	0.4272	725	0.0008	1.601	199.2	1.292	1.022	151.3
4.08	14.70	2046	1114.8	24.532	1.2342	0.4269	721	0.0008	1.615	199.7	1.305	1.028	152.3
10.00	6.00	1721	978.3	24.532	1.2448	0.4119	641	0.0003	2.155	219.7	2.187	1.264	187.3
20.00	3.00	1499	888.0	24.532	1.2540	0.3999	581	0.0009	2.546	232.7	3.443	1.399	207.2
40.00	1.50	1300	809.6	24.532	1.2646	0.3872	523	0.0006	2.931	243.6	5.545	1.506	223.1
100.00	.60	1068	721.9	24.532	1.2800	0.3703	450	0.0001	3.451	255.3	10.611	1.617	239.5
200.00	.30	916	666.3	24.532	1.2924	0.3580	398	0.0008	3.863	262.4	17.467	1.684	249.4
400.00	.15	781	618.8	24.532	1.3056	0.3460	349	0.0006	4.298	268.3	28.839	1.739	257.6
1000.00	.06	627	566.7	24.532	1.3230	0.3318	289	0.0003	4.924	274.5	56.029	1.798	266.3
2000.00	.03	528	534.3	24.532	1.3355	0.3224	249	0.0001	5.446	278.3	92.556	1.853	271.5
4000.00	.02	443	507.2	24.532	1.3475	0.3142	212	0.0009	6.016	281.5	152.735	1.882	275.8

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(e) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P_e	Static pressure, P_e , lb./sq. in. abs.	Temperature, T_e , °K	Enthalpy, h_e , cal/g	Molecular weight, M_e	Isentropic exponent, γ_e	Specific heat, C_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number M_e	Specific impulse in vacuum, I_{vac} , (lb)(sec)/lb	Area ratio, A_e	Thrust coefficient, C_F	Specific impulse, I , (lb)(sec)/(lb)
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	60.00	2347	1054.4	26.257	1.2321	0.4017	798	0.00040	0.000	306.9	2.188	0.000	0.0
1.05	57.14	2326	1045.8	26.257	1.2326	.4010	794	.00039	.282	306.9	2.188	.204	27.4
1.20	50.00	2268	1022.6	26.257	1.2339	.3992	781	.00039	.548	194.5	1.269	.392	52.6
1.40	42.86	2202	996.5	26.257	1.2355	.3971	766	.00038	.750	173.1	1.066	.529	71.0
1.60	37.50	2147	974.5	26.257	1.2368	.3955	754	.00037	.892	168.2	1.011	.621	83.4
1.80	33.42	2100	956.0	26.257	1.2380	.3937	743	.00036	1.000	167.3	1.000	.690	92.5
2.00	30.00	2057	939.0	26.257	1.2391	.3922	733	.00036	1.094	167.8	1.008	.747	100.2
4.00	15.00	1796	838.1	26.257	1.2469	.3822	669	.00032	1.998	180.3	1.285	1.023	137.2
4.08	14.70	1789	835.3	26.257	1.2471	.3819	667	.00032	1.611	180.7	1.298	1.029	138.1
10.00	6.00	1493	724.3	26.257	1.2585	.3685	588	.00027	2.155	198.5	2.162	1.263	169.5
20.00	3.00	1292	651.4	26.257	1.2684	.3577	530	.00024	2.549	210.0	3.387	1.396	187.3
40.00	1.50	1113	588.3	26.257	1.2793	.3467	475	.00021	2.941	219.6	5.428	1.501	201.4
100.00	.60	908	518.5	26.257	1.2950	.3323	406	.00017	3.471	229.8	10.316	1.610	215.9
200.00	.30	773	474.5	26.257	1.3079	.3215	357	.00015	3.893	236.0	16.892	1.674	224.6
400.00	.15	655	437.1	26.257	1.3212	.3113	312	.00013	4.342	241.1	27.741	1.728	231.8
1000.00	.06	522	396.4	26.257	1.3386	.2992	258	.00010	4.990	246.5	53.515	1.784	239.3
2000.00	.03	437	371.3	26.257	1.3510	.2913	221	.00009	5.531	249.7	87.939	1.817	243.8
4000.00	.02	364	350.4	26.257	1.3601	.2859	187	.00007	6.129	252.3	144.427	1.845	247.5
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	60.00	2062	855.0	27.299	1.2440	0.3711	740	0.00034	0.000	282.0	2.195	0.000	0.0
1.05	57.14	2042	847.7	27.299	1.2445	.3705	735	.00034	.281	282.0	2.195	.205	25.2
1.20	50.00	1989	828.1	27.299	1.2459	.3688	722	.00033	.546	178.6	1.272	.394	48.4
1.40	42.86	1929	806.1	27.299	1.2476	.3668	708	.00032	.747	158.9	1.068	.531	65.2
1.60	37.50	1879	787.6	27.299	1.2491	.3650	696	.00032	.888	154.3	1.012	.623	76.6
1.80	33.42	1835	771.5	27.299	1.2505	.3634	684	.00031	1.000	153.4	1.000	.694	85.2
2.00	30.00	1797	757.8	27.299	1.2517	.3620	675	.00031	1.090	153.8	1.007	.748	92.0
4.00	15.00	1560	673.2	27.299	1.2600	.3528	612	.00027	1.994	165.1	1.279	1.024	125.8
4.08	14.70	1554	670.9	27.299	1.2603	.3525	610	.00027	1.607	165.4	1.292	1.030	126.6
10.00	6.00	1287	578.5	27.299	1.2725	.3399	534	.00023	2.154	181.4	2.138	1.262	155.1
20.00	3.00	1107	518.2	27.299	1.2850	.3300	479	.00020	2.553	191.7	3.333	1.393	171.2
40.00	1.50	948	466.4	27.299	1.2943	.3201	427	.00018	2.950	200.2	5.313	1.496	183.9
100.00	.60	766	409.5	27.299	1.3111	.3068	363	.00014	3.491	209.2	10.027	1.602	196.9
200.00	.30	648	373.8	27.299	1.3244	.2972	317	.00012	3.924	214.6	16.328	1.665	204.6
400.00	.15	545	343.8	27.299	1.3380	.2881	276	.00010	4.387	219.1	26.662	1.716	210.9
1000.00	.06	431	311.4	27.299	1.3550	.2779	226	.00008	5.058	223.8	51.055	1.770	217.5
2000.00	.03	359	291.5	27.299	1.3642	.2726	192	.00007	5.625	226.6	83.484	1.802	221.4
4000.00	.02	298	275.0	27.299	1.3704	.2693	162	.00006	6.250	228.8	136.601	1.828	224.7

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P	Static pressure, P, lb/in ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse, I _{sp} , (lb)(sec)/lb	Area ratio, E	Thrust coefficient, C _F	Specific impulse, I
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	150.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000			0.000	0.0
1.05	142.86	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	0.271	530.1	2.250	0.210	47.4
1.20	125.00	1129	5218.8	4.416	1.3436	1.7597	303	0.00070	0.27	534.2	1.297	0.403	90.8
1.40	107.14	1085	5141.8	4.416	1.3469	1.7472	293	0.00068	0.22	536.1	1.081	0.543	122.2
1.60	93.75	1049	5077.7	4.416	1.3497	1.7369	285	0.00066	0.80	538.6	1.018	0.636	143.2
1.85	80.42	1008	5006.8	4.416	1.3528	1.7257	276	0.00063	1.000	541.1	1.000	0.725	163.4
2.00	75.00	989	4975.4	4.416	1.3540	1.7210	274	0.00062	1.059	544.4	1.003	0.761	171.5
4.00	37.50	824	4693.4	4.416	1.3651	1.6825	234	0.00052	1.566	551.7	1.233	1.031	232.3
10.00	15.00	645	4392.5	4.416	1.3748	1.6505	188	0.00042	2.152	527.5	1.974	1.257	283.1
10.21	14.70	639	4386.6	4.416	1.3770	1.6501	187	0.00041	2.165	528.1	1.997	1.261	284.0
20.00	7.50	552	4209.8	4.416	1.3799	1.6344	159	0.00035	2.586	543.5	2.982	1.376	309.9
40.00	3.75	439	4058.9	4.416	1.3824	1.6268	133	0.00029	3.031	556.4	4.620	1.467	330.4
100.00	1.50	340	3899.0	4.416	1.3882	1.6093	104	0.00023	3.648	569.8	8.432	1.558	350.8
200.00	0.75	280	3802.6	4.416	1.3926	1.5961	85	0.00018	4.149	577.7	13.431	1.610	362.6
400.00	0.38	230	3723.2	4.416	1.4008	1.5862	70	0.00015	4.675	584.1	21.488	1.652	372.0
1000.00	0.15	175	3640.1	4.416	1.4349	1.4847	55	0.00011	5.438	590.6	39.928	1.694	381.6
2000.00	0.08	142	3590.9	4.416	1.4550	1.4389	45	0.00009	6.096	594.3	62.572	1.719	387.2
4000.00	0.04	114	3551.2	4.416	1.4705	1.4065	36	0.00007	6.845	597.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	150.00	1514	2969.7	5.216	1.3079	1.6183	402	0.00084	0.000			0.000	0.0
1.05	142.86	1497	2941.7	5.216	1.3090	1.6140	399	0.00083	0.274	552.2	2.233	0.209	49.3
1.20	125.00	1430	2866.8	5.216	1.3120	1.6022	389	0.00081	0.333	548.6	1.289	0.400	94.6
1.40	107.14	1398	2785.2	5.216	1.3155	1.5887	378	0.00078	0.730	559.3	1.077	0.539	127.4
1.60	93.75	1354	2713.2	5.216	1.3185	1.5772	369	0.00076	0.869	569.6	1.016	0.632	149.4
1.85	81.25	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	577.3	1.000	0.716	169.2
2.00	75.00	1282	2601.1	5.216	1.3236	1.5584	353	0.00072	1.088	587.8	1.004	0.757	179.1
4.00	37.50	1079	2290.0	5.216	1.3391	1.5046	307	0.00061	1.572	516.7	1.244	1.029	243.2
10.00	15.00	852	1924.3	5.216	1.3576	1.4516	251	0.00048	2.146	544.7	2.009	1.257	297.2
10.21	14.70	847	1917.7	5.216	1.3592	1.4506	250	0.00048	2.161	545.3	2.033	1.261	298.2
20.00	7.50	709	1748.8	5.216	1.3656	1.4252	215	0.00040	2.573	562.0	3.049	1.379	325.9
40.00	3.75	588	1578.0	5.216	1.3715	1.4066	179	0.00034	3.010	576.0	4.739	1.472	348.0
100.00	1.50	458	1396.3	5.216	1.3771	1.3913	142	0.00026	3.619	590.5	8.679	1.565	370.0
200.00	0.75	379	1266.2	5.216	1.3811	1.3807	117	0.00022	4.111	599.1	15.870	1.619	382.7
400.00	0.38	312	1195.2	5.216	1.3881	1.3677	96	0.00018	4.638	606.1	22.295	1.662	392.9
1000.00	0.15	242	1099.0	5.216	1.3973	1.3400	74	0.00013	5.394	613.4	41.979	1.706	403.5
2000.00	0.08	198	1041.1	5.216	1.4156	1.2977	61	0.00011	6.014	617.6	67.687	1.733	409.6
4000.00	0.04	161	993.9	5.216	1.4350	1.2568	50	0.00009	6.704	621.1	108.754	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	150.00	1816	1249.3	6.016	1.2035	1.4955	481	0.00092	0.000			0.000	0.0
1.05	142.86	1797	1220.2	6.016	1.2044	1.4917	477	0.00091	0.276	563.4	2.219	0.207	50.3
1.20	125.00	1744	1142.1	6.016	1.2070	1.4812	467	0.00089	0.328	558.1	1.283	0.398	96.6
1.40	107.14	1685	1054.8	6.016	1.2100	1.4693	456	0.00086	0.736	563.3	1.073	0.536	130.1
1.60	93.75	1635	981.5	6.016	1.2127	1.4590	446	0.00085	0.876	568.6	1.015	0.629	152.6
1.85	81.25	1586	910.0	6.016	1.2194	1.4466	436	0.00081	1.000	574.5	1.000	0.708	171.6
2.00	75.00	1554	864.0	6.016	1.2273	1.4415	429	0.00080	1.076	581.1	1.003	0.754	183.1
4.00	37.50	1322	555.3	6.016	1.3125	1.3673	378	0.00068	1.576	525.5	1.256	1.027	249.3
10.00	15.00	1057	176.5	6.016	1.3330	1.3225	314	0.00054	2.147	555.3	2.048	1.258	303.5
10.21	14.70	1052	169.3	6.016	1.3334	1.3212	312	0.00054	2.159	555.8	2.072	1.263	305.5
20.00	7.50	887	9954.4	6.016	1.3401	1.2848	269	0.00046	2.583	573.6	3.127	1.382	332.7
40.00	3.75	740	9788.6	6.016	1.3509	1.2559	220	0.00038	2.987	586.6	4.883	1.478	358.9
100.00	1.50	580	9587.7	6.016	1.3605	1.2320	181	0.00030	3.581	604.1	8.985	1.575	382.3
200.00	0.75	481	9448.5	6.016	1.3717	1.2191	151	0.00023	4.064	613.3	14.395	1.630	395.9
400.00	0.38	399	9348.0	6.016	1.3755	1.2100	124	0.00020	4.582	620.8	23.206	1.675	406.7
1000.00	0.15	310	9241.3	6.016	1.3821	1.1946	95	0.00015	5.327	628.7	43.889	1.722	418.0
2000.00	0.08	256	9176.7	6.016	1.3885	1.1805	78	0.00012	5.965	633.3	71.271	1.749	424.7
4000.00	0.04	210	9123.5	6.016	1.4039	1.1482	64	0.00010	6.606	637.1	115.534	1.771	430.1
R = 0.300, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	150.00	2092	9932.7	6.813	1.2648	1.3932	550	0.00097	0.000			0.000	0.0
1.05	142.86	2071	9903.1	6.813	1.2655	1.3901	546	0.00096	0.278	568.3	2.208	0.206	50.8
1.20	125.00	2013	9823.6	6.813	1.2676	1.3814	536	0.00094	0.32	559.6	1.278	0.396	97.5
1.40	107.14	1949	9734.3	6.813	1.2702	1.3711	524	0.00091	0.741	569.6	1.071	0.533	131.3
1.60	93.75	1894	9639.7	6.813	1.2725	1.3619	514	0.00089	0.881	570.0	1.013	0.626	154.1
1.85	81.25	1843	9590.2	6.813	1.2748	1.3530	504	0.00087	1.000	570.1	1.000	0.701	172.6
2.00	75.00	1805	9539.4	6.813	1.2765	1.3463	497	0.00085	1.082	580.8	1.006	0.752	185.0
4.00	37.50	1549	9200.9	6.813	1.2895	1.2976	444	0.00074	1.585	530.2	1.266	1.025	252.4
10.00	15.00	1254	8827.4	6.813	1.3099	1.2529	374	0.00060	2.146	581.4	2.084	1.260	310.1
10.21	14.70	1248	8819.9	6.813	1.3105	1.2515	373	0.00060	2.166	582.1	2.110	1.264	311.2
20.00	7.50	1081	8593.8	6.813	1.3222	1.1885	324	0.00050	2.555	586.8	3.204	1.386	341.3
40.00	3.75	893	8396.8	6.813	1.3307	1.1527	278	0.00042	2.965	596.6	5.034	1.485	363.6
100.00	1.50	705	8184.1	6.813	1.3533	1.1172	223	0.00035	3.545	613.0	9.516	1.584	390.1
200.00	0.75	588	8033.8	6.813	1.3608	1.1005	186	0.00027	4.014	622.8	14.981	1.642	404.3
400.00	0.38	488	7942.3	6.813	1.3688	1.0866	155	0.00023	4.518	630.5	24.213	1.689	415.9
1000.00	0.15	381	7829.0	6.813	1.3720	1.0745	120	0.00017	5.249	639.1	45.957	1.738	427.8
2000.00	0.08	316	7739.4	6.813	1.3776	1.0630	97	0.00014	5.954	644.1	74.439	1.766	434.9
4000.00	0.04	261	7701.3	6.813	1.3831	1.0530	80	0.00011	6.722	646.2	122.076	1.790	440.6

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb/sq in abs	Temperature, T , K	Enthalpy, h , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , (lb)(sec)/lb	Area ratio, ϵ	Thrust coefficient, C_F	Specific impulse, I , (lb)(sec)/lb
R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	150.00	2339	8892.6	7.604	1.2505	1.3047	610	0.00099	0.000	569.0	2.199	0.000	0.0
1.05	142.86	2310	8863.1	7.604	1.2511	1.3020	608	+00099	+280	569.0	2.199	+205	50.8
1.20	125.00	2254	8783.4	7.604	1.2529	1.2980	598	+00097	+544	560.3	1.274	+394	97.6
1.40	107.14	2183	8693.9	7.604	1.2551	1.2859	584	+00094	+745	550.4	1.069	+532	131.5
1.60	93.75	2120	8616.7	7.604	1.2570	1.2784	574	+00092	+886	541.0	1.012	+624	154.4
1.80	82.97	2074	8551.7	7.604	1.2587	1.2715	564	+00090	+1000	530.2	1.000	+696	172.3
2.00	75.00	2031	8497.5	7.604	1.2602	1.2656	556	+00089	+1087	510.0	1.007	+749	185.5
4.00	37.50	1796	8154.9	7.604	1.2720	1.2443	502	+00078	+1590	532.2	1.274	+1024	253.4
10.00	15.00	1436	7773.7	7.604	1.2899	1.1627	431	+00064	2.150	564.4	2.115	1.261	312.1
10.21	14.70	1430	7760.0	7.604	1.2904	1.1614	429	+00064	2.162	565.0	2.142	1.265	313.1
20.00	7.50	1225	7532.9	7.604	1.3050	1.1182	377	+00055	2.551	584.5	3.274	1.390	344.0
40.00	3.75	1039	7328.2	7.604	1.3202	1.0774	326	+00046	2.955	601.0	5.175	1.491	369.0
100.00	1.50	828	7103.5	7.604	1.3377	1.0353	264	+00036	3.514	618.2	9.648	1.594	394.4
200.00	.75	694	6968.0	7.604	1.3485	1.0112	223	+00030	3.969	628.5	15.575	1.654	409.2
400.00	.38	579	6823.0	7.604	1.3563	.9948	186	+00025	4.459	636.9	25.259	1.703	421.3
1000.00	.15	494	6729.9	7.604	1.3642	.9790	146	+00019	5.169	645.7	48.098	1.753	433.8
2000.00	.08	417	6654.8	7.604	1.3692	.9693	119	+00015	5.760	651.0	78.522	1.783	441.3
4000.00	.04	312	6592.5	7.604	1.3742	.9598	97	+00012	6.403	655.3	128.377	1.808	447.4
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	150.00	2551	8050.5	8.379	1.2395	1.2276	660	0.00101	0.000	566.4	2.192	0.000	0.0
1.05	142.86	2527	8021.1	8.379	1.2400	1.2254	658	+00100	+281	566.4	2.192	+205	50.6
1.20	125.00	2464	7942.1	8.379	1.2415	1.2192	646	+00098	+547	558.9	1.271	+393	97.1
1.40	107.14	2391	7853.3	8.379	1.2435	1.2118	634	+00096	+748	549.3	1.067	+530	131.0
1.60	93.75	2327	7776.6	8.379	1.2450	1.2052	624	+00094	+889	540.1	1.012	+623	153.8
1.80	85.31	2276	7714.2	8.379	1.2465	1.1992	615	+00092	+1000	530.3	1.000	+692	171.1
2.00	75.00	2229	7658.0	8.379	1.2479	1.1938	607	+00090	+1091	519.2	1.007	+748	184.8
4.00	37.50	1958	7516.0	8.379	1.2578	1.1570	553	+00080	1.594	531.9	1.280	1.023	252.8
10.00	15.00	1599	6932.6	8.379	1.2738	1.1033	480	+00067	2.152	564.8	2.141	1.262	311.9
10.21	14.70	1592	6924.9	8.379	1.2742	1.1021	479	+00067	2.163	565.4	2.168	1.267	313.0
20.00	7.50	1373	6688.7	8.379	1.2879	1.0609	425	+00058	2.548	585.4	3.332	1.393	344.2
40.00	3.75	1173	6479.7	8.379	1.3030	1.0200	371	+00049	2.944	602.4	5.298	1.496	369.7
100.00	1.50	943	6250.6	8.379	1.3224	.9728	304	+00039	3.490	620.3	9.946	1.602	395.7
200.00	.75	794	6108.2	8.379	1.3351	.9448	258	+00032	3.931	631.0	16.131	1.664	411.1
400.00	.38	666	5988.4	8.379	1.3455	.9235	217	+00026	4.406	639.8	26.255	1.714	423.6
1000.00	.15	525	5859.6	8.379	1.3562	.9029	170	+00020	5.095	649.0	50.189	1.757	436.6
2000.00	.08	437	5780.8	8.379	1.3517	.8928	141	+00017	5.672	654.5	82.113	1.799	444.4
4000.00	.04	365	5715.2	8.379	1.3570	.8833	115	+00014	6.299	659.1	134.543	1.824	450.8
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	150.00	2733	7354.5	9.133	1.2310	1.1595	701	0.00100	0.000	561.5	2.187	0.000	0.0
1.05	142.86	2708	7325.0	9.133	1.2315	1.1576	698	+00100	+282	561.5	2.187	+204	50.1
1.20	125.00	2640	7247.9	9.133	1.2328	1.1521	688	+00098	+549	555.9	1.269	+392	96.3
1.40	107.14	2564	7160.6	9.133	1.2344	1.1459	676	+00096	+750	546.8	1.066	+529	129.9
1.60	93.75	2500	7087.1	9.133	1.2358	1.1404	666	+00094	+892	537.7	1.011	+621	152.5
1.79	85.35	2446	7025.3	9.133	1.2371	1.1355	657	+00092	+1000	528.0	1.000	+689	169.2
2.00	75.00	2395	6968.2	9.133	1.2383	1.1307	649	+00091	+1094	517.0	1.008	+747	183.3
4.00	37.50	2092	6830.2	9.133	1.2471	1.0962	593	+00082	1.597	529.9	1.285	1.023	251.0
10.00	15.00	1738	6249.2	9.133	1.2614	1.0500	522	+00069	2.153	563.2	2.161	1.263	310.1
10.21	14.70	1730	6241.5	9.133	1.2617	1.0489	521	+00069	2.165	563.8	2.189	1.268	311.2
20.00	7.50	1501	6005.3	9.133	1.2741	1.0114	467	+00060	2.546	584.1	3.379	1.396	342.6
40.00	3.75	1289	5795.1	9.133	1.2884	.9720	411	+00051	2.937	601.5	5.399	1.500	368.4
100.00	1.50	1045	5563.1	9.133	1.3084	.9231	341	+00041	3.471	619.9	10.202	1.608	394.8
200.00	.75	885	5417.9	9.133	1.3224	.8924	291	+00034	3.901	630.9	16.618	1.672	410.5
400.00	.38	745	5295.2	9.133	1.3349	.8675	246	+00028	4.362	640.0	27.151	1.724	423.3
1000.00	.15	590	5162.6	9.133	1.3475	.8438	194	+00022	5.033	649.5	52.106	1.779	436.7
2000.00	.08	493	5081.2	9.133	1.3553	.8300	162	+00018	5.595	655.2	85.445	1.812	444.8
4000.00	.04	410	5013.2	9.133	1.3608	.8207	132	+00014	6.207	660.0	140.259	1.838	451.4
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	150.00	2881	6769.6	9.859	1.2244	1.0999	736	0.00099	0.000	554.9	2.183	0.000	0.0
1.05	142.86	2855	6741.4	9.859	1.2248	1.0981	732	+00099	+283	554.9	2.183	+204	49.5
1.20	125.00	2785	6665.5	9.859	1.2260	1.0932	722	+00097	+550	551.8	1.267	+392	95.2
1.40	107.14	2707	6580.2	9.859	1.2275	1.0875	710	+00095	+752	543.3	1.065	+528	126.4
1.60	93.75	2641	6508.2	9.859	1.2288	1.0824	700	+00093	+894	534.4	1.011	+620	150.8
1.79	85.79	2586	6447.1	9.859	1.2299	1.0783	692	+00092	+1000	524.8	1.000	+687	167.0
2.00	75.00	2533	6391.5	9.859	1.2310	1.0741	683	+00091	+1096	515.8	1.008	+746	181.3
4.00	37.50	2220	6060.2	9.859	1.2389	1.0492	630	+00082	1.600	526.8	1.289	1.022	248.5
10.00	15.00	1894	5684.8	9.859	1.2517	1.0024	558	+00070	2.154	560.2	2.177	1.264	307.2
10.21	14.70	1886	5677.1	9.859	1.2520	1.0014	556	+00070	2.166	560.8	2.205	1.268	308.3
20.00	7.50	1609	5443.2	9.859	1.2653	.9570	502	+00061	2.545	581.3	3.416	1.398	339.7
40.00	3.75	1388	5234.1	9.859	1.2788	.9297	445	+00053	2.932	598.8	5.481	1.504	365.5
100.00	1.50	1122	5001.9	9.859	1.2984	.8817	372	+00042	3.457	617.5	10.413	1.613	392.2
200.00	.75	963	4855.8	9.859	1.3112	.8493	320	+00035	3.878	628.8	17.030	1.679	408.1
400.00	.38	815	4731.0	9.859	1.3247	.8223	272	+00029	4.328	638.1	27.924	1.732	421.1
1000.00	.15	648	4597.2	9.859	1.3395	.7953	218	+00023	4.982	647.9	53.794	1.789	434.8
2000.00	.08	543	4514.2	9.859	1.3485	.7799	180	+00019	5.529	653.5	88.422	1.822	443.0
4000.00	.04	453	4444.8	9.859	1.3554	.7687	149	+00015	6.128	658.6	145.411	1.850	449.8

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXIGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(f) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _e /P	Static pressure, P, lb/sq in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb)(sec)/lb	Area ratio, ε	Thrust coefficient, C _f	Specific impulse, I, (lb)(sec)/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	150.00	3097	5841.5	11.228	1.2152	0.9999	788	0.00096	0.000			0.000	0.0
1.05	142.86	3070	5815.0	11.228	1.2155	.9981	789	.00096	.284			.203	46.1
1.20	125.00	2998	5743.3	11.228	1.2186	.9942	774	.00094	.352	539.3	2.177	.391	92.5
1.40	107.14	2917	5662.6	11.228	1.2178	.9895	763	.00092	.755	342.1	1.264	.527	124.8
1.60	93.75	2846	5594.5	11.228	1.2189	.9853	753	.00091	.897	304.8	1.064	.619	146.6
1.78	84.08	2793	5540.1	11.228	1.2199	.9819	745	.00090	1.000	294.7	1.000	.684	162.0
2.00	75.00	2736	5484.2	11.228	1.2209	.9782	736	.00088	1.100	285.8	1.009	.744	176.3
4.00	37.50	2410	5169.0	11.228	1.2275	.9590	683	.00080	1.603	318.6	1.295	1.021	241.9
10.00	15.00	2027	4809.9	11.228	1.2306	.9197	611	.00070	2.155	351.7	2.199	1.263	299.6
10.21	14.70	2019	4802.6	11.228	1.2306	.9189	610	.00070	2.167	352.4	2.228	1.269	300.7
20.00	7.50	1770	4577.3	11.228	1.2405	.8893	555	.00062	2.543	372.8	3.469	1.400	331.7
40.00	3.75	1536	4374.7	11.228	1.2602	.8572	498	.00054	2.925	390.4	5.598	1.508	357.3
100.00	1.50	1266	4147.8	11.228	1.2785	.8128	423	.00044	3.439	409.3	10.724	1.621	383.9
200.00	.75	1086	4003.7	11.228	1.2933	.7804	368	.00037	3.846	420.8	17.650	1.688	399.9
400.00	.38	925	3880.6	11.228	1.3000	.7516	316	.00031	4.280	430.3	29.113	1.744	413.1
1000.00	.15	742	3745.9	11.228	1.3257	.7204	253	.00024	4.907	440.4	56.470	1.803	427.0
2000.00	.08	624	3662.3	11.228	1.3366	.7028	212	.00020	5.433	446.5	93.204	1.838	435.5
4000.00	.04	523	3592.1	11.228	1.3459	.6886	176	.00016	6.008	451.5	153.804	1.868	442.4
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	150.00	3231	5138.3	12.482	1.2096	0.9187	825	0.00092	0.000			0.000	0.0
1.05	142.86	3203	5113.3	12.482	1.2099	.9175	822	.00092	.285			.203	46.6
1.20	125.00	3130	5046.0	12.482	1.2108	.9143	811	.00090	.353	331.5	2.174	.390	89.6
1.40	107.14	3049	4970.2	12.482	1.2119	.9105	800	.00089	.756	295.4	1.063	.526	120.9
1.60	93.75	2976	4905.4	12.482	1.2129	.9070	789	.00088	.899	267.2	1.010	.618	142.1
1.78	84.26	2921	4850.1	12.482	1.2137	.9041	781	.00088	1.000	258.8	1.000	.682	156.7
2.00	75.00	2862	4802.5	12.482	1.2146	.9009	773	.00085	1.102	248.9	1.009	.744	170.9
4.00	37.50	2528	4505.4	12.482	1.2206	.8810	720	.00078	1.605	309.3	1.299	1.021	234.7
10.00	15.00	2136	4165.8	12.482	1.2306	.8504	648	.00068	2.156	341.8	2.213	1.266	290.9
10.21	14.70	2128	4158.8	12.482	1.2306	.8497	647	.00068	2.168	342.4	2.242	1.270	291.9
20.00	7.50	1873	3944.8	12.482	1.2393	.8244	592	.00061	2.542	362.5	3.502	1.402	322.3
40.00	3.75	1634	3751.6	12.482	1.2500	.7960	535	.00053	2.920	380.0	5.671	1.511	347.4
100.00	1.50	1394	3534.1	12.482	1.2670	.7556	459	.00044	3.427	398.7	10.922	1.620	372.6
200.00	.75	1167	3395.2	12.482	1.2813	.7251	402	.00037	3.828	410.2	18.053	1.694	389.5
400.00	.38	999	3275.9	12.482	1.2963	.6964	348	.00031	4.251	419.7	29.905	1.751	402.6
1000.00	.15	806	3144.6	12.482	1.3131	.6664	282	.00024	4.861	429.9	58.305	1.812	416.5
2000.00	.08	681	3062.8	12.482	1.3276	.6451	237	.00020	5.371	438.1	96.550	1.849	425.0
4000.00	.04	573	2993.8	12.482	1.3381	.6300	198	.00016	5.930	441.2	159.767	1.879	432.0
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	150.00	3304	4586.9	13.622	1.2063	0.8531	851	0.00088	0.000			0.000	0.0
1.05	142.86	3277	4563.5	13.622	1.2066	.8520	847	.00088	.285			.203	45.1
1.20	125.00	3202	4500.4	13.622	1.2075	.8491	837	.00086	.354	321.0	1.262	.390	86.8
1.40	107.14	3118	4429.3	13.622	1.2084	.8458	825	.00085	.757	286.1	1.062	.526	117.1
1.60	93.75	3047	4369.2	13.622	1.2093	.8428	815	.00084	.900	278.2	1.010	.618	137.6
1.78	84.26	2992	4322.8	13.622	1.2101	.8403	807	.00083	1.000	270.9	1.000	.681	151.6
2.00	75.00	2932	4271.9	13.622	1.2109	.8374	798	.00081	1.103	277.9	1.009	.743	165.5
4.00	37.50	2595	3992.0	13.622	1.2186	.8195	745	.00075	1.606	299.8	1.301	1.021	227.4
10.00	15.00	2198	3673.1	13.622	1.2296	.7825	673	.00066	2.156	331.5	2.222	1.266	282.0
10.21	14.70	2190	3666.5	13.622	1.2296	.7819	671	.00066	2.168	332.1	2.251	1.271	283.0
20.00	7.50	1931	3465.5	13.622	1.2340	.7694	617	.00059	2.541	351.7	3.522	1.405	312.5
40.00	3.75	1690	3281.6	13.622	1.2441	.7436	559	.00052	2.918	368.8	5.715	1.513	337.0
100.00	1.50	1405	3075.1	13.622	1.2601	.7068	483	.00043	3.421	387.3	11.092	1.628	362.7
200.00	.75	1214	2942.8	13.622	1.2739	.6785	425	.00037	3.817	398.6	18.300	1.698	378.2
400.00	.38	1043	2828.9	13.622	1.2880	.6510	370	.00031	4.234	408.0	30.397	1.756	391.1
1000.00	.15	845	2703.0	13.622	1.3060	.6195	302	.00024	4.834	418.1	59.488	1.818	404.9
2000.00	.08	716	2624.3	13.622	1.3214	.5998	255	.00020	5.334	424.2	98.706	1.855	413.2
4000.00	.04	603	2557.7	13.622	1.3327	.5844	214	.00016	5.862	429.3	163.055	1.887	420.2
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	150.00	3336	4142.9	14.653	1.2044	0.7990	870	0.00084	0.000			0.000	0.0
1.05	142.86	3308	4121.0	14.653	1.2047	.7981	866	.00084	.285			.203	45.7
1.20	125.00	3234	4061.7	14.653	1.2056	.7954	855	.00083	.354	311.0	1.262	.390	86.1
1.40	107.14	3150	3992.0	14.653	1.2065	.7923	843	.00081	.758	277.3	1.062	.525	113.5
1.60	93.75	3078	3938.6	14.653	1.2074	.7896	832	.00080	.900	269.6	1.009	.618	133.3
1.78	84.26	3024	3895.3	14.653	1.2081	.7874	824	.00079	1.000	268.3	1.000	.680	146.8
2.00	75.00	2962	3847.2	14.653	1.2089	.7848	815	.00078	1.104	269.4	1.009	.743	160.4
4.00	37.50	2625	3584.9	14.653	1.2143	.7684	761	.00071	1.607	290.6	1.302	1.021	220.4
10.00	15.00	2227	3284.0	14.653	1.2290	.7438	689	.00063	2.157	321.5	2.226	1.266	273.4
10.21	14.70	2219	3277.8	14.653	1.2290	.7432	687	.00063	2.168	322.1	2.256	1.271	274.4
20.00	7.50	1957	3087.4	14.653	1.2310	.7227	632	.00056	2.541	341.2	3.533	1.404	303.1
40.00	3.75	1716	2914.8	14.653	1.2408	.6968	575	.00050	2.916	357.9	5.740	1.514	326.9
100.00	1.50	1431	2719.7	14.653	1.2592	.6620	498	.00042	3.417	375.9	11.109	1.630	351.9
200.00	.75	1230	2594.4	14.653	1.2797	.6385	440	.00036	3.811	387.0	18.439	1.700	367.1
400.00	.38	1060	2480.3	14.653	1.2944	.6125	383	.00030	4.223	398.2	30.678	1.759	379.9
1000.00	.15	865	2366.6	14.653	1.3207	.5822	315	.00024	4.819	408.1	60.145	1.821	393.1
2000.00	.08	734	2291.6	14.653	1.3374	.5630	268	.00020	5.313	412.2	99.576	1.859	401.4
4000.00	.04	620	2228.1	14.653	1.3522	.5476	225	.00016	5.855	417.1	165.972	1.891	408.2

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(r) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/in ² abs	Temp-erature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb)(sec)/lb	Area ratio, ε	Thrust coefficient, C _f	Specific impulse, I, (lb)(sec)/lb
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	150.00	3341	3777.9	15.586	1.2035	0.7539	882	0.00061	0.000			0.000	0.0
1.05	142.86	3313	3757.2	15.586	1.2036	0.7540	878	0.00060	0.003	475.5	2.170	0.202	37.6
1.20	125.00	3239	3701.4	15.586	1.2040	0.7500	866	0.00079	0.254	30.0	1.461	0.389	81.6
1.40	107.14	3155	3630.6	15.586	1.2050	0.7477	855	0.00098	0.758	60.1	1.062	0.523	110.1
1.60	93.75	3084	3585.5	15.586	1.2064	0.7452	845	0.00076	0.901	61.0	1.009	0.617	129.4
1.78	84.45	3029	3544.7	15.586	1.2071	0.7432	836	0.00075	1.000	60.4	1.000	0.680	142.4
2.00	75.00	2968	3499.4	15.586	1.2079	0.7407	827	0.00074	1.104	61.4	1.009	0.743	155.7
4.00	37.50	2631	3252.2	15.586	1.2132	0.7254	772	0.00068	1.607	62.1	1.303	1.021	317.9
10.00	15.00	2234	2968.5	15.586	1.2217	0.7025	699	0.00060	2.157	61.1	2.228	1.266	265.4
10.21	14.70	2226	2962.7	15.586	1.2219	0.7019	697	0.00060	2.168	61.7	2.258	1.271	266.3
20.00	7.50	1967	2783.1	15.586	1.2276	0.6826	642	0.00054	2.340	61.5	3.539	1.404	294.2
40.00	3.75	1724	2620.1	15.586	1.2322	0.6606	584	0.00048	2.715	64.5	5.752	1.512	317.6
100.00	1.50	1439	2435.8	15.586	1.2393	0.6289	507	0.00040	3.416	65.1	11.143	1.631	341.7
200.00	0.75	1246	2317.3	15.586	1.2475	0.6041	450	0.00034	3.808	65.9	18.509	1.701	326.5
400.00	0.38	1074	2214.9	15.586	1.2540	0.5796	394	0.00029	4.221	66.9	30.821	1.760	368.8
1000.00	0.15	873	2101.5	15.586	1.3013	0.5207	324	0.00023	4.812	67.6	60.493	1.822	381.9
2000.00	0.08	741	2030.3	15.586	1.3150	0.5222	276	0.00019	5.303	68.5	100.644	1.861	390.6
4000.00	0.04	626	1970.0	15.586	1.3271	0.5173	233	0.00016	5.841	69.4	167.211	1.893	396.6
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	150.00	3219	2626.1	19.176	1.2047	0.6098	905	0.00067	0.000			0.000	0.0
1.05	142.86	3193	2609.9	19.176	1.2050	0.6091	901	0.00067	0.285	420.8	2.171	0.203	37.6
1.20	125.00	3121	2566.2	19.176	1.2058	0.6071	890	0.00066	0.554	267.1	1.262	0.389	81.6
1.40	107.14	3040	2517.0	19.176	1.2068	0.6047	876	0.00064	0.758	238.1	1.062	0.523	97.4
1.60	93.75	2971	2475.4	19.176	1.2077	0.6026	865	0.00063	0.900	231.5	1.010	0.618	114.5
1.78	84.45	2918	2443.4	19.176	1.2084	0.6008	856	0.00063	1.000	230.4	1.000	0.680	126.1
2.00	75.00	2859	2408.0	19.176	1.2093	0.5988	846	0.00062	1.103	231.3	1.009	0.743	137.7
4.00	37.50	2532	2214.6	19.176	1.2147	0.5863	787	0.00056	1.607	249.6	1.302	1.021	189.2
10.00	15.00	2148	1992.8	19.176	1.2235	0.5674	710	0.00049	2.157	276.0	2.225	1.266	234.7
10.21	14.70	2140	1986.2	19.176	1.2237	0.5669	708	0.00049	2.168	276.5	2.255	1.271	235.6
20.00	7.50	1865	1847.9	19.176	1.2314	0.5315	621	0.00044	2.341	292.9	3.531	1.404	260.2
40.00	3.75	1635	1720.8	19.176	1.2408	0.5340	592	0.00039	2.717	307.2	5.736	1.514	280.7
100.00	1.50	1380	1577.0	19.176	1.2557	0.5089	515	0.00033	3.419	322.7	11.104	1.630	302.1
200.00	0.75	1195	1484.7	19.176	1.2664	0.4898	458	0.00028	3.813	332.2	18.438	1.700	315.1
400.00	0.38	1029	1404.9	19.176	1.2823	0.4708	403	0.00024	4.227	340.2	30.698	1.758	326.0
1000.00	0.15	837	1316.6	19.176	1.3007	0.4482	334	0.00019	4.819	348.7	60.267	1.821	337.5
2000.00	0.08	711	1261.1	19.176	1.3141	0.4336	287	0.00016	5.311	353.9	100.302	1.859	344.6
4000.00	0.04	601	1214.1	19.176	1.3263	0.4212	244	0.00013	5.848	358.2	166.710	1.891	350.5
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	150.00	3045	2016.0	21.610	1.2087	0.5325	900	0.00058	0.000			0.000	0.0
1.05	142.86	3020	2002.4	21.610	1.2091	0.5318	896	0.00058	0.285	385.5	2.173	0.203	34.4
1.20	125.00	2921	1965.8	21.610	1.2100	0.5299	884	0.00057	0.553	244.6	1.263	0.390	66.1
1.40	107.14	2873	1924.5	21.610	1.2111	0.5278	870	0.00056	0.756	218.0	1.063	0.526	89.2
1.60	93.75	2806	1889.6	21.610	1.2121	0.5255	858	0.00055	0.899	211.9	1.010	0.618	104.9
1.78	84.45	2755	1862.4	21.610	1.2129	0.5238	848	0.00054	1.000	210.9	1.000	0.682	115.6
2.00	75.00	2699	1833.2	21.610	1.2139	0.5220	838	0.00053	1.102	211.7	1.009	0.744	126.1
4.00	37.50	2385	1671.3	21.610	1.2196	0.5106	777	0.00045	1.605	226.3	1.295	1.021	173.2
10.00	15.00	2017	1486.2	21.610	1.2289	0.4937	697	0.00042	2.156	252.3	2.215	1.266	214.7
10.21	14.70	2009	1482.4	21.610	1.2291	0.4933	695	0.00042	2.168	252.8	2.244	1.270	215.5
20.00	7.50	1769	1365.7	21.610	1.2374	0.4733	637	0.00038	2.342	267.6	3.508	1.402	237.9
40.00	3.75	1546	1260.1	21.610	1.2470	0.4643	577	0.00033	2.721	280.6	5.665	1.512	256.5
100.00	1.50	1284	1141.2	21.610	1.2619	0.4430	501	0.00028	3.427	294.5	10.972	1.626	275.9
200.00	0.75	1109	1065.1	21.610	1.2746	0.4269	445	0.00024	3.826	303.1	18.118	1.696	287.7
400.00	0.38	952	999.5	21.610	1.2878	0.4114	392	0.00021	4.246	310.2	30.400	1.753	297.4
1000.00	0.15	772	927.1	21.610	1.3057	0.3927	326	0.00017	4.847	317.9	59.148	1.815	307.8
2000.00	0.08	655	881.7	21.610	1.3187	0.3805	281	0.00014	5.346	322.5	98.282	1.852	314.2
4000.00	0.04	552	843.3	21.610	1.3307	0.3700	240	0.00012	5.891	326.4	163.108	1.883	319.4
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	150.00	2695	1381.4	24.614	1.2194	0.4488	859	0.00047	0.000			0.000	0.0
1.05	142.86	2672	1370.8	24.614	1.2198	0.4481	855	0.00047	0.285	237.8	2.160	0.203	30.3
1.20	125.00	2608	1342.4	24.614	1.2209	0.4463	842	0.00046	0.551	125.5	1.266	0.391	58.3
1.40	107.14	2556	1310.4	24.614	1.2221	0.4442	828	0.00045	0.754	121.9	1.064	0.527	78.6
1.60	93.75	2475	1265.3	24.614	1.2235	0.4423	815	0.00044	0.896	116.5	1.010	0.620	92.4
1.78	84.45	2426	1261.5	24.614	1.2243	0.4407	805	0.00044	1.000	115.6	1.000	0.685	102.1
2.00	75.00	2376	1239.7	24.614	1.2255	0.4391	795	0.00043	1.098	116.2	1.008	0.745	111.1
4.00	37.50	2089	1114.9	24.614	1.2322	0.4265	731	0.00039	1.602	120.5	1.293	1.022	152.3
10.00	15.00	1752	973.1	24.614	1.2427	0.4134	649	0.00033	2.155	221.1	2.219	1.265	188.5
10.21	14.70	1745	970.2	24.614	1.2430	0.4130	647	0.00033	2.167	221.6	2.245	1.269	189.2
20.00	7.50	1527	881.5	24.614	1.2518	0.4014	589	0.00029	2.343	234.3	3.521	1.399	208.6
40.00	3.75	1326	801.7	24.614	1.2621	0.3887	530	0.00026	2.730	245.3	5.655	1.507	224.6
100.00	1.50	1071	712.6	24.614	1.2775	0.3710	457	0.00022	3.446	257.1	10.899	1.610	241.2
200.00	0.75	956	655.7	24.614	1.2897	0.3594	405	0.00019	3.858	264.3	17.963	1.658	252.3
400.00	0.38	799	607.4	24.614	1.3020	0.3474	356	0.00016	4.291	270.5	29.027	1.711	259.5
1000.00	0.15	643	554.3	24.614	1.3201	0.3269	295	0.00012	4.914	276.7	56.470	1.800	266.3
2000.00	0.08	542	521.2	24.614	1.3325	0.3235	254	0.00010	5.431	280.5	92.373	1.825	273.6
4000.00	0.04	453	493.3	24.614	1.3449	0.3148	218	0.00009	5.977	282.7	154.220	1.865	278.0

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(r) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute; Frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb./sq. in. abs.	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g. K.)	Viscosity, μ , micro-poses	Thermal conductivity, k, cal/(sec. K. m)	Mach number, M	Specific impulse, I _{vac} , in vacuum, lb.-sec./lb.	Area ratio, ϵ	Thrust coefficient, C _f	Specific impulse, I, lb.-sec./lb.
R = 4.000, PERCENT FUEL = 5.054, O/F = 31.766													
1.00	150.00	2363	1054.4	26.281	1.2315	0.4922	804	0.00070	0.000	0.000	2.187	0.000	0.0
1.05	162.85	2391	1094.7	26.287	1.2314	0.4915	797	0.00070	0.262	307.7	2.187	0.204	27.5
1.20	189.00	2283	1022.4	26.287	1.2332	0.4971	754	0.00077	0.348	175.0	1.289	0.394	24.6
1.40	197.14	2217	990.2	26.287	1.2348	0.4976	710	0.00080	0.755	73.0	1.068	0.527	21.2
1.60	232.75	2101	974.1	26.287	1.2361	0.4971	657	0.00077	0.872	60.0	1.011	0.621	18.6
1.79	252.58	2114	952.2	26.287	1.2373	0.4962	640	0.00076	1.000	67.7	1.000	0.694	17.7
2.00	270.00	2071	930.4	26.287	1.2384	0.4957	639	0.00076	1.074	66.3	1.006	0.747	16.5
4.00	37.50	1807	836.9	26.287	1.2461	0.4927	673	0.00052	1.578	180.0	1.289	1.022	137.6
R = 10.000, PERCENT FUEL = 5.054, O/F = 31.766													
10.00	15.00	1507	722.4	26.287	1.2576	0.4891	751	0.00077	2.155	179.1	2.189	1.253	170.6
10.21	16.70	1498	720.0	26.287	1.2579	0.4897	749	0.00077	2.166	175.7	2.192	1.258	170.5
20.00	7.50	1303	648.3	26.287	1.2679	0.4862	733	0.00074	2.747	210.6	3.091	1.376	167.3
40.00	3.75	1123	585.3	26.287	1.2763	0.4842	710	0.00071	2.940	220.3	5.435	1.504	162.0
R = 100.000, PERCENT FUEL = 5.054, O/F = 31.766													
100.00	1.50	916	515.0	26.287	1.2974	0.4826	707	0.00077	3.470	230.5	10.234	1.540	151.6
200.00	0.75	780	470.7	26.287	1.3086	0.4807	700	0.00077	3.891	236.8	16.929	1.679	145.0
400.00	0.38	661	433.0	26.287	1.3188	0.4791	697	0.00077	4.239	241.9	27.812	1.728	138.5
R = 1000.000, PERCENT FUEL = 5.054, O/F = 31.766													
1000.00	0.15	527	352.0	26.287	1.3375	0.4776	690	0.00077	4.962	247.2	53.579	1.794	130.1
2000.00	0.08	442	300.0	26.287	1.3504	0.4759	683	0.00077	5.323	250.6	86.240	1.818	124.5
4000.00	0.04	366	242.3	26.287	1.3574	0.4753	687	0.00077	6.121	253.2	144.979	1.846	118.8
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.663													
1.00	150.00	2066	855.0	27.307	1.2456	0.5712	741	0.00044	0.000	0.000	2.194	0.000	0.0
1.05	162.86	2047	847.7	27.307	1.2453	0.5708	736	0.00044	0.261	282.3	2.194	0.207	25.2
1.20	189.00	1974	826.1	27.307	1.2457	0.5707	724	0.00043	0.348	176.0	1.412	0.394	22.6
1.40	197.14	1934	808.0	27.307	1.2474	0.5699	709	0.00042	0.747	159.1	1.068	0.527	19.2
1.60	232.75	1883	787.2	27.307	1.2489	0.5691	697	0.00042	0.888	134.4	1.012	0.623	16.6
1.79	252.58	1837	771.3	27.307	1.2503	0.5683	686	0.00041	1.000	133.6	1.000	0.694	15.7
2.00	270.00	1801	757.6	27.307	1.2519	0.5681	676	0.00041	1.070	124.0	1.007	0.748	14.4
4.00	37.50	1504	672.0	27.307	1.2576	0.5647	613	0.00047	1.574	189.2	1.287	1.022	123.7
R = 10.000, PERCENT FUEL = 2.458, O/F = 39.663													
10.00	15.00	1290	577.9	27.307	1.2762	0.5601	733	0.00043	2.154	181.6	2.189	1.256	133.2
10.21	16.70	1264	576.0	27.307	1.2763	0.5598	734	0.00043	2.166	181.9	2.192	1.257	133.2
20.00	7.50	1110	517.5	27.307	1.2867	0.5562	700	0.00040	2.753	191.6	3.094	1.376	127.6
40.00	3.75	950	465.6	27.307	1.2940	0.5523	673	0.00038	2.940	200.4	5.425	1.504	124.1
R = 100.000, PERCENT FUEL = 2.458, O/F = 39.663													
100.00	1.50	769	408.3	27.307	1.3106	0.5489	703	0.00044	3.471	237.4	10.232	1.540	117.1
200.00	0.75	650	372.8	27.307	1.3241	0.5473	693	0.00043	3.924	244.0	16.927	1.679	110.6
400.00	0.38	547	342.6	27.307	1.3377	0.5453	676	0.00040	4.239	249.3	26.603	1.717	104.1
R = 1000.000, PERCENT FUEL = 2.458, O/F = 39.663													
1000.00	0.15	452	310.1	27.307	1.3574	0.5412	671	0.00040	5.057	249.0	51.132	1.770	97.7
2000.00	0.08	360	290.2	27.307	1.3660	0.5407	673	0.00037	5.623	246.8	83.267	1.802	92.7
4000.00	0.04	279	252.6	27.307	1.3703	0.5403	664	0.00036	6.121	243.1	136.764	1.826	87.3

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_e/P_c	Static pressure, P_c , lb./sq. in. abs.	Temp. erature, T, K	Enthalpy, h_c , cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(K)(cm)	Mach number, M	Specific impulse, I_{sp} , in vacuum, lb.(sec)/lb.	Area ratio, E	Thrust coefficient, C_f	Specific impulse, I_{sp} , lb.(sec)/lb.
R = 0.150, PERCENT FUEL = 45.65, O/F = 1.190													
1.00	300.00	1181	5511.5	4.416	1.3396	1.7753	314	0.00073	0.000	0.000	0.000	0.000	0.0
1.05	285.71	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	0.271	330.0	2.2501	1.210	47.4
1.20	250.00	1127	5210.6	4.416	1.3436	1.7597	303	0.00070	0.247	334.2	1.2977	1.403	90.8
1.40	214.29	1065	5141.8	4.416	1.3489	1.7472	293	0.00066	0.222	346.1	1.001	1.543	122.2
1.60	187.50	1009	5071.7	4.416	1.3477	1.7369	285	0.00066	0.200	356.6	1.018	1.636	143.2
1.87	160.84	1006	5006.6	4.416	1.3528	1.7257	276	0.00063	1.000	364.1	1.000	1.729	163.2
2.00	150.00	989	4975.4	4.416	1.3570	1.7210	272	0.00062	1.059	368.4	1.003	1.761	171.5
4.00	75.00	824	4693.4	4.416	1.3691	1.6825	254	0.00052	1.566	301.7	1.233	1.031	232.3
10.00	30.00	603	4392.3	4.416	1.3798	1.6509	230	0.00042	2.152	247.5	1.974	1.257	253.1
20.00	15.00	522	4278.8	4.416	1.3777	1.6394	229	0.00033	2.986	243.5	2.982	1.376	309.9
20.41	14.70	529	4204.2	4.416	1.3661	1.6340	228	0.00035	2.999	243.9	3.020	1.379	310.6
40.00	7.50	459	4038.9	4.416	1.3624	1.6268	223	0.00029	3.031	256.4	4.020	1.467	330.4
100.00	3.00	340	3699.0	4.416	1.3662	1.6073	194	0.00023	3.648	269.6	6.452	1.558	350.8
200.00	1.50	280	3602.6	4.416	1.3726	1.5961	82	0.00018	4.149	277.7	13.431	1.610	362.6
400.00	0.75	230	3723.2	4.416	1.4098	1.5562	70	0.00015	4.675	284.1	21.488	1.652	372.0
1000.00	0.30	175	3640.1	4.416	1.4349	1.4847	55	0.00011	5.438	290.6	39.928	1.694	381.6
2000.00	0.15	142	3590.9	4.416	1.4550	1.4389	45	0.00009	6.296	294.3	63.572	1.719	387.2
4000.00	0.08	114	3551.2	4.416	1.4705	1.4065	36	0.00007	6.845	297.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, O/F = 1.587													
1.00	300.00	1514	2869.7	5.216	1.3079	1.6183	402	0.00084	0.000	0.000	0.000	0.000	0.0
1.05	285.71	1497	2911.7	5.216	1.3070	1.6140	399	0.00083	0.274	352.2	2.233	1.209	49.3
1.20	250.00	1400	2856.8	5.216	1.3120	1.6022	389	0.00081	0.233	348.6	1.289	1.400	94.6
1.40	214.29	1330	2783.2	5.216	1.3125	1.5887	378	0.00078	0.250	359.3	1.077	1.539	127.4
1.60	187.50	1254	2713.2	5.216	1.3185	1.5772	369	0.00076	0.269	299.6	1.016	1.632	149.6
1.87	162.47	1207	2640.5	5.216	1.3217	1.5621	359	0.00073	1.000	297.3	1.000	1.716	169.2
2.00	150.00	1262	2601.1	5.216	1.3255	1.5504	353	0.00072	1.058	297.8	1.004	1.757	179.1
4.00	75.00	1079	2290.0	5.216	1.3391	1.5046	307	0.00061	1.572	316.7	1.244	1.029	243.2
10.00	30.00	852	1954.3	5.216	1.3528	1.4516	271	0.00048	2.148	344.7	2.009	1.257	297.2
20.00	15.00	709	1748.8	5.216	1.3626	1.4232	213	0.00040	2.973	325.0	3.049	1.379	325.9
20.41	14.70	705	1743.3	5.216	1.3636	1.4225	212	0.00040	2.986	325.4	3.088	1.382	326.7
40.00	7.50	586	1578.0	5.216	1.3713	1.4066	179	0.00034	3.010	376.0	4.759	1.472	340.0
100.00	3.00	428	1396.3	5.216	1.3711	1.3915	142	0.00026	3.619	390.3	6.679	1.563	370.0
200.00	1.50	379	1286.2	5.216	1.3611	1.3807	117	0.00022	4.111	399.3	13.570	1.619	362.7
400.00	0.75	312	1192.2	5.216	1.3681	1.3677	96	0.00018	4.632	406.1	22.496	1.662	372.9
1000.00	0.30	242	1097.0	5.216	1.3973	1.3400	74	0.00013	5.394	412.4	41.979	1.706	403.5
2000.00	0.15	198	1041.1	5.216	1.4126	1.2977	61	0.00011	6.014	417.7	67.667	1.733	409.5
4000.00	0.08	161	993.9	5.216	1.4320	1.2508	50	0.00009	6.704	421.1	108.754	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, O/F = 1.984													
1.00	300.00	1817	1249.3	6.016	1.2835	1.4955	481	0.00092	0.000	0.000	0.000	0.000	0.0
1.05	285.71	1797	1220.2	6.016	1.2844	1.4917	477	0.00091	0.276	363.4	2.219	1.207	50.3
1.20	250.00	1745	1142.1	6.016	1.2930	1.4813	467	0.00089	0.238	356.2	1.283	1.396	96.6
1.40	214.29	1663	1094.5	6.016	1.2930	1.4693	456	0.00086	0.256	316.3	1.073	1.539	130.1
1.60	187.50	1632	981.5	6.016	1.2977	1.4591	446	0.00083	0.276	306.6	1.019	1.632	152.6
1.87	162.47	1586	909.9	6.016	1.2974	1.4485	436	0.00081	1.000	304.9	1.000	1.706	171.8
2.00	150.00	1524	884.0	6.016	1.2973	1.4442	427	0.00080	1.076	303.1	1.003	1.734	181.1
4.00	75.00	1222	732.2	6.016	1.3123	1.3873	376	0.00068	1.579	325.9	1.266	1.027	249.3
10.00	30.00	1037	576.3	6.016	1.3269	1.3223	314	0.00054	2.147	355.3	2.048	1.258	305.6
20.00	15.00	887	4954.3	6.016	1.3481	1.2846	269	0.00046	2.963	373.6	3.127	1.382	335.7
20.41	14.70	882	4948.3	6.016	1.3484	1.2839	267	0.00045	2.975	374.1	3.167	1.386	336.5
40.00	7.50	740	4768.5	6.016	1.3509	1.2657	229	0.00038	2.987	388.6	4.883	1.476	359.6
100.00	3.00	580	4569.5	6.016	1.3663	1.2320	181	0.00030	3.681	404.1	6.985	1.575	382.3
200.00	1.50	481	4448.3	6.016	1.3717	1.2194	151	0.00025	4.264	412.3	14.295	1.636	395.9
400.00	0.75	399	4347.6	6.016	1.3795	1.2100	124	0.00020	4.782	420.9	23.207	1.679	406.3
1000.00	0.30	310	4241.1	6.016	1.3884	1.1948	93	0.00015	5.327	426.7	43.070	1.722	415.0
2000.00	0.15	236	4176.3	6.016	1.3969	1.1805	78	0.00012	6.043	433.3	71.274	1.749	424.7
4000.00	0.08	210	4123.3	6.016	1.4037	1.1492	64	0.00010	6.906	437.1	115.639	1.771	430.1
R = 0.300, PERCENT FUEL = 29.57, O/F = 2.381													
1.00	300.00	2093	9932.7	6.814	1.2647	1.3933	550	0.00097	0.000	0.000	0.000	0.000	0.0
1.05	285.71	2072	9903.1	6.814	1.2655	1.3905	547	0.00096	0.278	366.3	2.208	1.205	50.3
1.20	250.00	2013	9823.3	6.814	1.2676	1.3816	536	0.00094	0.242	359.7	1.278	1.396	97.2
1.40	214.29	1950	9734.4	6.814	1.2701	1.3713	525	0.00091	0.261	319.7	1.071	1.533	131.4
1.60	187.50	1892	9639.6	6.814	1.2724	1.3621	514	0.00089	0.281	310.1	1.012	1.626	154.2
1.87	162.47	1844	9590.0	6.814	1.2747	1.3532	503	0.00087	1.000	308.2	1.000	1.701	172.5
2.00	150.00	1806	9534.2	6.814	1.2765	1.3469	497	0.00085	1.052	306.9	1.003	1.731	185.1
4.00	75.00	1520	9400.2	6.814	1.2920	1.2876	444	0.00074	1.593	320.3	1.266	1.029	252.4
10.00	30.00	1223	8266.7	6.814	1.3076	1.2331	375	0.00060	2.146	361.5	2.084	1.260	310.2
20.00	15.00	1024	6993.0	6.814	1.3291	1.1867	323	0.00050	2.925	380.9	3.123	1.387	341.4
20.41	14.70	1027	6987.7	6.814	1.3292	1.1874	323	0.00050	2.937	381.4	3.167	1.390	342.2
40.00	7.50	823	6392.6	6.814	1.3386	1.1576	278	0.00042	3.069	396.7	4.825	1.483	365.7
100.00	3.00	626	6163.0	6.814	1.3525	1.1172	223	0.00033	3.745	412.1	9.320	1.585	390.2
200.00	1.50	528	6052.6	6.814	1.3655	1.1005	186	0.00027	4.114	422.9	14.964	1.643	404.5
400.00	0.75	469	5944.0	6.814	1.3785	1.0866	158	0.00023	4.516	430.9	24.219	1.689	416.6
1000.00	0.30	352	5626.2	6.814	1.3925	1.0745	120	0.00017	5.246	439.2	45.968	1.738	427.9
2000.00	0.15	276	5577.9	6.814	1.3976	1.0640	98	0.00014	6.053	446.2	76.338	1.767	435.0
4000.00	0.08	251	5549.7	6.814	1.4050	1.0391	80	0.00011	6.912	448.3	122.092	1.790	440.8

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb./sq. in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c _p , cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec) °K/(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , lb.(sec)/lb.	Area ratio, E	Thrust coefficient, C _f	Specific impulse, I, lb.(sec)/lb.
R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	300.00	2344	8892.8	7.607	1.2502	1.3052	610	0.00100	0.000	269.5	2.199	0.000	0.0
1.05	285.71	2321	8863.0	7.607	1.2509	1.3025	607	0.00099	0.280	269.5	2.199	0.205	50.9
1.20	250.00	2259	8783.2	7.607	1.2527	1.2951	597	0.00097	0.345	260.6	1.276	0.394	97.7
1.40	214.29	2190	8693.6	7.607	1.2548	1.2864	585	0.00094	0.745	220.7	1.069	0.532	131.6
1.60	187.50	2131	8618.2	7.607	1.2567	1.2789	575	0.00092	0.886	211.3	1.012	0.624	154.6
1.81	165.96	2079	8551.1	7.607	1.2584	1.2720	565	0.00090	1.000	209.4	1.000	0.696	172.4
2.00	150.00	2036	8496.8	7.607	1.2600	1.2661	557	0.00089	1.087	210.3	1.007	0.749	185.6
4.00	75.00	1760	8153.6	7.607	1.2717	1.2229	503	0.00078	1.590	232.5	1.274	1.024	253.6
10.00	30.00	1440	7771.6	7.607	1.2896	1.1634	432	0.00064	2.150	264.7	2.116	1.261	312.3
20.00	15.00	1229	7530.3	7.607	1.3046	1.1108	378	0.00055	2.351	284.9	3.275	1.390	344.3
20.41	14.70	1223	7523.7	7.607	1.3051	1.1175	377	0.00054	2.363	285.4	3.319	1.394	345.1
40.00	7.50	1042	7325.1	7.607	1.3199	1.0779	327	0.00046	2.954	401.4	5.178	1.491	369.3
100.00	3.00	831	7101.8	7.607	1.3374	1.0396	265	0.00036	3.514	418.7	9.654	1.594	394.8
200.00	1.50	696	6963.9	7.607	1.3482	1.0114	223	0.00030	3.968	429.0	15.587	1.654	409.7
400.00	0.75	581	6846.6	7.607	1.3560	0.9949	187	0.00025	4.457	437.4	25.280	1.703	421.7
1000.00	0.30	456	6725.1	7.607	1.3639	0.9790	146	0.00019	5.168	446.2	48.144	1.754	434.3
2000.00	0.15	378	6649.8	7.607	1.3690	0.9693	119	0.00015	5.738	451.5	78.603	1.784	441.8
4000.00	0.08	314	6587.3	7.607	1.3740	0.9598	97	0.00012	6.400	455.8	128.518	1.808	447.9
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	300.00	2565	8050.5	8.389	1.2389	1.2285	662	0.00101	0.000	267.5	2.192	0.000	0.0
1.05	285.71	2541	8021.0	8.389	1.2394	1.2265	658	0.00100	0.281	267.5	2.192	0.205	50.7
1.20	250.00	2476	7941.7	8.389	1.2409	1.2202	646	0.00098	0.347	259.2	1.271	0.393	97.3
1.40	214.29	2403	7852.6	8.389	1.2427	1.2128	636	0.00096	0.748	219.9	1.067	0.530	131.2
1.60	187.50	2341	7777.6	8.389	1.2444	1.2062	626	0.00094	0.889	210.6	1.012	0.622	154.1
1.81	165.96	2287	7713.0	8.389	1.2459	1.2005	617	0.00092	1.000	208.9	1.000	0.692	171.4
2.00	150.00	2240	7656.5	8.389	1.2473	1.1949	609	0.00091	1.091	209.8	1.007	0.748	185.2
4.00	75.00	1948	7315.1	8.389	1.2571	1.1582	555	0.00081	1.594	232.6	1.281	1.023	253.3
10.00	30.00	1608	6928.0	8.389	1.2750	1.1047	482	0.00068	2.152	265.6	2.142	1.262	312.5
20.00	15.00	1382	6682.9	8.389	1.2870	1.0523	427	0.00058	2.348	286.3	3.335	1.393	345.0
20.41	14.70	1376	6676.2	8.389	1.2874	1.0511	426	0.00058	2.360	286.8	3.380	1.397	345.8
40.00	7.50	1180	6472.9	8.389	1.3020	1.0213	373	0.00049	2.944	403.3	5.305	1.496	370.5
100.00	3.00	949	6242.4	8.389	1.3215	0.9738	306	0.00039	3.488	421.3	9.963	1.602	396.6
200.00	1.50	800	6099.1	8.389	1.3345	0.9455	260	0.00032	3.929	432.1	16.162	1.664	412.1
400.00	0.75	671	5978.6	8.389	1.3448	0.9239	219	0.00027	4.403	440.9	26.311	1.715	424.6
1000.00	0.30	529	5849.0	8.389	1.3526	0.9031	171	0.00021	5.091	450.1	50.311	1.768	437.7
2000.00	0.15	441	5769.6	8.389	1.3582	0.8926	142	0.00017	5.667	455.7	82.327	1.799	445.5
4000.00	0.08	366	5703.5	8.389	1.3665	0.8833	116	0.00014	6.293	460.3	134.918	1.825	451.9
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	300.00	2755	7354.5	9.152	1.2300	1.1611	705	0.00101	0.000	263.2	2.186	0.000	0.0
1.05	285.71	2730	7325.4	9.152	1.2305	1.1591	701	0.00100	0.282	263.2	2.186	0.204	50.3
1.20	250.00	2682	7247.2	9.152	1.2318	1.1537	691	0.00098	0.349	257.0	1.268	0.392	96.6
1.40	214.29	2606	7159.4	9.152	1.2334	1.1475	679	0.00096	0.751	217.8	1.066	0.529	130.3
1.60	187.50	2521	7085.4	9.152	1.2348	1.1420	669	0.00095	0.892	208.7	1.011	0.621	153.0
1.79	167.23	2467	7023.4	9.152	1.2352	1.1372	661	0.00093	1.000	207.0	1.000	0.689	169.7
2.00	150.00	2416	6965.8	9.152	1.2352	1.1324	652	0.00092	1.094	208.0	1.008	0.747	183.9
4.00	75.00	2112	6625.4	9.152	1.2459	1.1000	599	0.00082	1.598	231.1	1.286	1.022	251.9
10.00	30.00	1755	6241.6	9.152	1.2600	1.0523	526	0.00070	2.153	264.5	2.163	1.263	311.2
20.00	15.00	1517	5995.6	9.152	1.2726	1.0138	471	0.00060	2.346	285.5	3.364	1.396	343.9
20.41	14.70	1511	5988.9	9.152	1.2730	1.0126	469	0.00060	2.358	286.1	3.431	1.399	344.7
40.00	7.50	1304	5783.6	9.152	1.2868	0.9743	415	0.00052	2.936	403.0	5.411	1.501	369.7
100.00	3.00	1057	5549.4	9.152	1.3067	0.9251	344	0.00041	3.469	421.5	10.232	1.609	396.3
200.00	1.50	898	5404.6	9.152	1.3208	0.8939	295	0.00034	3.898	432.7	16.676	1.673	412.1
400.00	0.75	755	5278.6	9.152	1.3334	0.8664	249	0.00028	4.357	441.8	27.260	1.725	425.0
1000.00	0.30	599	5144.5	9.152	1.3462	0.8443	197	0.00022	5.026	451.4	52.343	1.780	438.5
2000.00	0.15	500	5062.0	9.152	1.3543	0.8300	164	0.00018	5.584	457.2	85.868	1.813	446.6
4000.00	0.08	417	4992.2	9.152	1.3596	0.8207	134	0.00015	6.196	462.0	141.008	1.840	453.3
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	300.00	2915	6769.6	9.891	1.2250	1.1020	741	0.00100	0.000	257.3	2.182	0.000	0.0
1.05	285.71	2889	6741.2	9.891	1.2254	1.1002	737	0.00100	0.283	257.3	2.182	0.204	49.8
1.20	250.00	2819	6664.6	9.891	1.2266	1.0933	727	0.00098	0.350	253.4	1.267	0.391	95.4
1.40	214.29	2741	6578.5	9.891	1.2281	1.0866	719	0.00096	0.752	214.7	1.065	0.528	129.0
1.60	187.50	2674	6502.9	9.891	1.2293	1.0806	709	0.00094	0.894	205.8	1.011	0.620	151.5
1.79	167.23	2619	6446.5	9.891	1.2294	1.0804	707	0.00093	1.000	204.2	1.000	0.687	167.7
2.00	150.00	2565	6388.5	9.891	1.2295	1.0763	699	0.00091	1.097	205.2	1.008	0.746	182.1
4.00	75.00	2220	6053.6	9.891	1.2372	1.0418	636	0.00083	1.600	228.4	1.290	1.022	249.6
10.00	30.00	1881	5674.2	9.891	1.2497	1.0025	564	0.00071	2.154	262.0	2.180	1.264	308.7
20.00	15.00	1633	5429.8	9.891	1.2611	0.9702	508	0.00062	2.345	283.3	3.424	1.398	341.4
20.41	14.70	1627	5423.1	9.891	1.2615	0.9692	506	0.00062	2.356	283.8	3.471	1.401	342.3
40.00	7.50	1411	5210.1	9.891	1.2744	0.9321	421	0.00053	2.931	401.0	5.497	1.504	367.4
100.00	3.00	1122	4962.7	9.891	1.2950	0.8848	376	0.00043	3.494	419.9	10.438	1.614	394.3
200.00	1.50	961	4834.4	9.891	1.3067	0.8516	326	0.00036	3.873	431.3	17.118	1.680	410.4
400.00	0.75	831	4708.4	9.891	1.3163	0.8242	277	0.00030	4.321	440.7	28.092	1.734	423.5
1000.00	0.30	602	4571.5	9.891	1.3373	0.7762	221	0.00023	4.771	450.6	54.169	1.791	437.3
2000.00	0.15	505	4467.0	9.891	1.3460	0.7606	184	0.00019	5.215	456.6	89.096	1.825	445.7
4000.00	0.08	403	4410.2	9.891	1.3538	0.7468	152	0.00016	5.711	461.5	146.602	1.853	452.5

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P	Static pressure, P, lb/in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, Cp, cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb)(sec)/lb	Area ratio, E	Thrust coefficient, C _F	Specific impulse, I, (lb)(sec)/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	300.00	3155	5841.6	11.290	1.2131	1.0021	796	0.00097	0.080	542.8	2.170	0.000	0.0
1.05	285.71	3128	5814.0	11.290	1.2134	1.0008	793	0.00097	0.284	544.4	1.264	0.003	45.4
1.20	250.00	3070	5742.0	11.290	1.2144	0.9970	783	0.00095	0.552	544.4	1.053	0.007	93.1
1.40	214.29	2973	5660.2	11.290	1.2156	0.9924	771	0.00093	0.755	540.0	1.003	0.012	123.6
1.60	187.50	2903	5591.2	11.290	1.2167	0.9883	761	0.00092	0.898	498.6	1.010	0.019	147.0
1.78	168.82	2840	5550.4	11.290	1.2170	0.9849	753	0.00091	1.000	490.0	1.000	0.023	162.9
2.00	150.00	2790	5479.4	11.290	1.2166	0.9813	744	0.00089	1.100	477.5	1.009	0.044	177.5
4.00	75.00	2460	5159.5	11.290	1.2249	0.9585	692	0.00082	1.604	320.9	1.296	1.021	245.6
10.00	30.00	2073	4794.7	11.290	1.2354	0.9258	621	0.00071	2.155	354.4	2.204	1.265	301.8
20.00	15.00	1812	4558.0	11.290	1.2452	0.8940	565	0.00063	2.542	375.7	3.481	1.401	334.2
20.41	14.70	1805	4551.5	11.290	1.2455	0.8930	564	0.00063	2.554	376.3	3.530	1.404	335.0
40.00	7.50	1577	4351.5	11.290	1.2565	0.8622	509	0.00055	2.723	393.6	5.624	1.509	360.1
100.00	3.00	1302	4119.9	11.290	1.2742	0.8178	433	0.00045	3.434	412.0	10.795	1.622	387.1
200.00	1.50	1118	3972.0	11.290	1.2890	0.7801	378	0.00038	3.839	424.5	17.754	1.601	403.3
400.00	0.75	954	3866.3	11.290	1.3038	0.7554	325	0.00032	4.270	434.2	29.356	1.747	416.7
1000.00	0.30	767	3708.0	11.290	1.3218	0.7250	262	0.00025	4.891	444.5	57.125	1.806	430.9
2000.00	0.15	646	3622.0	11.290	1.3331	0.7044	220	0.00020	5.411	450.7	94.401	1.842	439.5
4000.00	0.08	542	3549.6	11.290	1.3427	0.6876	183	0.00017	5.980	455.9	155.954	1.872	446.6
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	300.00	3307	5138.3	12.574	1.2069	0.9217	836	0.00094	0.000	526.7	2.172	0.000	0.0
1.05	285.71	3280	5112.9	12.574	1.2073	0.9205	832	0.00093	0.285	526.7	1.262	0.003	47.0
1.20	250.00	3205	5044.5	12.574	1.2082	0.9172	822	0.00092	0.554	534.3	1.062	0.007	90.3
1.40	214.29	3121	4987.4	12.574	1.2092	0.9136	810	0.00090	0.757	497.9	1.002	0.012	121.9
1.60	187.50	3049	4923.3	12.574	1.2101	0.9103	800	0.00089	0.900	489.6	1.010	0.018	145.3
1.78	168.82	2994	4851.8	12.574	1.2109	0.9075	794	0.00088	1.000	480.0	1.000	0.021	157.9
2.00	150.00	2933	4796.8	12.574	1.2118	0.9048	783	0.00086	1.103	489.4	1.009	0.043	172.4
4.00	75.00	2595	4494.4	12.574	1.2175	0.8847	731	0.00079	1.606	312.1	1.300	1.021	230.7
10.00	30.00	2197	4148.0	12.574	1.2267	0.8521	660	0.00070	2.156	343.0	2.220	1.066	293.5
20.00	15.00	1930	3922.2	12.574	1.2352	0.8299	605	0.00062	2.541	366.1	3.518	1.403	325.3
20.41	14.70	1922	3916.0	12.574	1.2355	0.8290	603	0.00062	2.552	366.6	3.567	1.406	326.1
40.00	7.50	1687	3724.3	12.574	1.2455	0.8017	548	0.00055	2.718	383.8	5.705	1.513	350.8
100.00	3.00	1402	3501.1	12.574	1.2618	0.7618	473	0.00045	3.422	403.0	11.013	1.628	377.4
200.00	1.50	1211	3358.2	12.574	1.2757	0.7312	416	0.00039	3.819	414.7	18.240	1.697	393.6
400.00	0.75	1039	3235.2	12.574	1.2906	0.7018	361	0.00032	4.238	424.5	30.278	1.755	406.9
1000.00	0.30	841	3099.5	12.574	1.3096	0.6684	294	0.00025	4.841	434.9	59.186	1.816	421.2
2000.00	0.15	712	3014.7	12.574	1.3227	0.6478	248	0.00021	5.343	441.2	96.189	1.838	429.5
4000.00	0.08	600	2943.0	12.574	1.3336	0.6318	207	0.00017	5.894	446.5	162.738	1.885	437.1
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	300.00	3393	4586.9	13.740	1.2033	0.8561	864	0.00090	0.000	510.4	2.170	0.000	0.0
1.05	285.71	3365	4563.0	13.740	1.2036	0.8551	860	0.00089	0.285	510.4	1.261	0.002	45.5
1.20	250.00	3290	4498.8	13.740	1.2044	0.8522	849	0.00088	0.555	524.0	1.061	0.007	87.6
1.40	214.29	3204	4426.4	13.740	1.2054	0.8488	837	0.00086	0.758	488.8	1.002	0.012	118.2
1.60	187.50	3132	4365.2	13.740	1.2062	0.8460	827	0.00085	0.901	480.8	1.009	0.017	138.9
1.78	168.82	3077	4318.3	13.740	1.2069	0.8437	819	0.00084	1.000	479.5	1.000	0.021	152.9
2.00	150.00	3015	4266.0	13.740	1.2077	0.8409	810	0.00083	1.104	480.6	1.009	0.043	167.1
4.00	75.00	2673	3981.2	13.740	1.2131	0.8234	758	0.00076	1.607	302.8	1.303	1.021	229.6
10.00	30.00	2270	3654.3	13.740	1.2216	0.7974	687	0.00067	2.157	335.0	2.229	1.266	284.9
20.00	15.00	1998	3440.7	13.740	1.2294	0.7750	632	0.00060	2.540	355.0	3.539	1.403	315.8
20.41	14.70	1990	3434.8	13.740	1.2297	0.7743	630	0.00060	2.551	356.2	3.590	1.406	316.6
40.00	7.50	1752	3252.9	13.740	1.2391	0.7496	570	0.00053	2.915	373.0	5.705	1.515	340.7
100.00	3.00	1462	3040.4	13.740	1.2542	0.7156	499	0.00045	3.416	391.9	11.146	1.631	366.8
200.00	1.50	1266	2903.8	13.740	1.2676	0.6852	441	0.00038	3.808	403.5	18.514	1.701	382.7
400.00	0.75	1091	2785.9	13.740	1.2822	0.6572	385	0.00032	4.220	413.2	30.827	1.760	395.9
1000.00	0.30	887	2655.2	13.740	1.3015	0.6243	316	0.00025	4.811	423.6	60.499	1.823	410.0
2000.00	0.15	753	2573.1	13.740	1.3153	0.6034	268	0.00021	5.303	429.9	100.640	1.861	418.6
4000.00	0.08	636	2503.6	13.740	1.3272	0.5867	226	0.00017	5.841	435.2	167.192	1.893	425.3
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	300.00	3430	4142.9	14.789	1.2013	0.8019	883	0.00086	0.000	494.7	2.169	0.000	0.0
1.05	285.71	3402	4120.6	14.789	1.2016	0.8010	879	0.00085	0.286	494.7	1.261	0.002	44.1
1.20	250.00	3327	4060.2	14.789	1.2024	0.7983	868	0.00084	0.555	514.0	1.061	0.007	84.3
1.40	214.29	3242	3992.2	14.789	1.2033	0.7955	856	0.00082	0.757	480.0	1.002	0.012	114.5
1.60	187.50	3169	3934.7	14.789	1.2041	0.7926	846	0.00081	0.901	474.2	1.009	0.017	134.6
1.77	169.04	3114	3890.9	14.789	1.2047	0.7900	838	0.00080	1.000	471.0	1.000	0.021	148.1
2.00	150.00	3051	3841.4	14.789	1.2055	0.7881	828	0.00079	1.105	472.1	1.010	0.043	162.0
4.00	75.00	2706	3573.5	14.789	1.2106	0.7722	775	0.00073	1.608	293.7	1.304	1.020	222.6
10.00	30.00	2305	3265.6	14.789	1.2186	0.7486	704	0.00065	2.157	325.0	2.234	1.267	276.3
20.00	15.00	2030	3084.0	14.789	1.2265	0.7261	645	0.00058	2.540	345.1	3.531	1.403	306.4
20.41	14.70	2023	3086.4	14.789	1.2268	0.7255	644	0.00058	2.551	345.7	3.602	1.406	307.2
40.00	7.50	1783	2866.6	14.789	1.2355	0.7045	581	0.00052	2.914	362.2	5.780	1.516	330.6
100.00	3.00	1491	2685.4	14.789	1.2501	0.6717	515	0.00045	3.412	380.6	11.219	1.635	356.1
200.00	1.50	1294	2529.9	14.789	1.2625	0.6421	457	0.00037	3.801	394.0	18.590	1.704	371.6
400.00	0.75	1117	2443.8	14.789	1.2773	0.6109	401	0.00032	4.211	401.5	31.135	1.763	384.5
1000.00	0.30	910	2315.3	14.789	1.2957	0.5782	331	0.00025	4.795	411.7	61.247	1.826	398.3
2000.00	0.15	775	2241.0	14.789	1.3097	0.5579	282	0.00021	5.280	417.9	102.025	1.868	406.8
4000.00	0.08	656	2174.5	14.789	1.3226	0.5422	238	0.00017	5.812	423.1	169.796	1.897	413.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Continued. Combustion-chamber pressure, 500 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb./sq.in. abs.	Temp-erature, T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g)(K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(K)(cm)	Mach number, M	Specific impulse, I _{vac} , lb.(sec)/lb.	Area ratio, ϵ	Thrust coefficient, C _f	Specific impulse, I, lb.(sec)/lb.
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	300.00	3437	3777.9	15.734	1.2004	0.7565	896	0.00084	0.000	480.1	2.168	0.204	0.0
1.05	285.71	3409	3756.8	15.734	1.2006	.7558	892	0.00081	.286	304.8	1.260	.389	37.9
1.20	250.00	3333	3699.9	15.734	1.2014	.7533	881	0.00080	.555	271.7	1.062	.525	111.2
1.40	214.29	3248	3625.9	15.734	1.2023	.7505	869	0.00078	.759	240.1	0.862	.617	130.7
1.60	187.50	3176	3561.7	15.734	1.2031	.7480	858	0.00076	.902	214.4	0.709	.679	145.7
1.75	169.41	3121	3520.6	15.734	1.2038	.7461	850	0.00075	1.000	187.9	0.617	.742	157.2
2.00	150.00	3058	3453.9	15.734	1.2045	.7439	841	0.00074	1.105	166.1	0.525	.742	157.2
4.00	75.00	2713	3241.4	15.734	1.2095	.7291	787	0.00070	1.608	68.1	1.303	1.020	216.1
10.00	30.00	2311	2951.0	15.734	1.2175	.7070	714	0.00064	2.157	25.6	1.256	1.409	297.5
20.00	15.00	2039	2780.8	15.734	1.2249	.6879	658	0.00058	2.340	13.1	3.557	1.409	297.5
20.41	14.70	2031	2755.6	15.734	1.2251	.6875	657	0.00058	2.351	13.7	3.607	1.409	298.3
40.00	7.50	1792	2593.3	15.734	1.2339	.6663	601	0.00050	2.913	5.17	5.792	1.516	321.0
100.00	3.00	1500	2403.2	15.734	1.2481	.6354	525	0.00042	3.410	369.7	11.253	1.633	345.8
200.00	1.50	1303	2280.7	15.734	1.2609	.6104	467	0.00036	3.799	380.8	18.738	1.705	360.9
400.00	.75	1126	2174.5	15.734	1.2749	.5857	410	0.00031	4.206	390.1	31.282	1.764	373.5
1000.00	.30	719	2026.5	15.734	1.2942	.5556	340	0.00024	4.788	400.1	61.611	1.828	387.0
2000.00	.15	703	1982.2	15.734	1.3083	.5360	291	0.00020	5.270	406.2	102.755	1.867	395.5
4000.00	.08	663	1919.0	15.734	1.3209	.5193	246	0.00017	5.798	411.2	171.104	1.899	402.2
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	300.00	3277	2626.1	19.320	1.2021	0.6117	918	0.00087	0.000	424.3	2.169	.204	0.0
1.05	285.71	3270	2609.6	19.320	1.2024	.6110	915	0.00087	.285	285.9	1.261	.389	37.9
1.20	250.00	3197	2559.2	19.320	1.2032	.6090	902	0.00086	.555	249.4	1.062	.525	72.6
1.40	214.29	3115	2513.1	19.320	1.2041	.6068	889	0.00085	.758	240.1	0.862	.617	98.2
1.60	187.50	3045	2472.8	19.320	1.2050	.6047	877	0.00084	.901	233.5	0.709	.679	115.5
1.75	169.41	2992	2440.6	19.320	1.2056	.6030	869	0.00084	1.000	224.4	0.617	.742	127.0
2.00	150.00	2911	2404.3	19.320	1.2065	.6011	858	0.00084	1.104	223.3	0.525	.742	138.9
4.00	75.00	2600	2207.3	19.320	1.2117	.5888	800	0.00079	1.608	85.9	1.303	1.020	190.9
10.00	30.00	2210	1981.0	19.320	1.2200	.5705	724	0.00073	2.157	27.7	2.232	1.256	236.9
20.00	15.00	1947	1832.9	19.320	1.2275	.5550	665	0.00067	2.340	13.9	3.546	1.409	262.7
20.41	14.70	1940	1826.8	19.320	1.2277	.5545	664	0.00067	2.351	14.5	3.597	1.408	263.4
40.00	7.50	1709	1702.7	19.320	1.2366	.5377	607	0.00061	2.915	5.04	5.769	1.515	283.4
100.00	3.00	1429	1555.2	19.320	1.2507	.5131	529	0.00053	3.414	326.2	11.194	1.632	305.3
200.00	1.50	1240	1460.2	19.320	1.2630	.4879	472	0.00047	3.805	335.9	18.624	1.703	314.5
400.00	.75	1070	1377.9	19.320	1.2766	.4747	416	0.00042	4.215	344.1	31.071	1.762	329.6
1000.00	.30	873	1285.6	19.320	1.2990	.4515	347	0.00037	4.800	352.8	61.164	1.825	341.4
2000.00	.15	743	1225.1	19.320	1.3087	.4361	299	0.00031	5.284	358.2	101.998	1.864	346.6
4000.00	.08	630	1180.2	19.320	1.3212	.4231	255	0.00026	5.814	362.6	169.845	1.896	354.7
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	300.00	3103	2015.0	21.723	1.2068	0.5339	910	0.00095	0.000	388.2	2.172	0.204	0.0
1.05	285.71	3077	2000.2	21.723	1.2071	.5335	908	0.00095	.285	263.4	1.262	.390	36.6
1.20	250.00	3007	1963.1	21.723	1.2080	.5314	898	0.00094	.554	219.6	1.064	.526	89.9
1.40	214.29	2928	1923.2	21.723	1.2090	.5291	886	0.00093	.757	219.6	0.864	.618	105.6
1.60	187.50	2861	1887.9	21.723	1.2100	.5271	875	0.00092	.900	213.4	0.710	.618	105.6
1.75	169.41	2809	1860.6	21.723	1.2108	.5250	865	0.00092	1.000	212.4	0.618	.681	116.4
2.00	150.00	2752	1830.6	21.723	1.2117	.5230	855	0.00092	1.103	213.3	0.526	.743	127.0
4.00	75.00	2435	1666.3	21.723	1.2173	.5125	787	0.00084	1.606	83.0	1.300	1.021	174.4
10.00	30.00	2082	1478.1	21.723	1.2263	.4958	708	0.00077	2.156	25.43	2.220	1.266	216.3
20.00	15.00	1811	1355.5	21.723	1.2344	.4817	648	0.00071	2.341	12.98	3.519	1.403	239.7
20.41	14.70	1804	1342.1	21.723	1.2347	.4813	646	0.00071	2.353	13.02	3.569	1.402	240.4
40.00	7.50	1565	1247.9	21.723	1.2427	.4668	586	0.00065	2.919	48.29	5.710	1.513	258.5
100.00	3.00	1319	1126.5	21.723	1.2583	.4456	511	0.00058	3.423	297.1	11.099	1.628	278.2
200.00	1.50	1141	1045.6	21.723	1.2706	.4292	453	0.00052	3.820	302.8	18.315	1.698	290.1
400.00	.75	962	981.4	21.723	1.2836	.4139	402	0.00046	4.237	313.1	30.473	1.756	300.0
1000.00	.30	798	931.1	21.723	1.3016	.3948	325	0.00041	4.833	320.9	59.799	1.818	310.6
2000.00	.15	677	883.4	21.723	1.3147	.3822	287	0.00036	5.326	325.6	99.507	1.856	317.1
4000.00	.08	572	820.8	21.723	1.3270	.3712	247	0.00031	5.865	329.6	165.365	1.887	322.5
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	300.00	2723	1581.4	24.659	1.2103	0.4495	905	0.00104	0.000	341.1	2.179	0.204	0.0
1.05	285.71	2699	1570.5	24.659	1.2107	.4488	903	0.00104	.284	241.1	1.265	.391	58.5
1.20	250.00	2635	1542.1	24.659	1.2118	.4470	888	0.00103	.551	216.3	1.065	.527	75.9
1.40	214.29	2563	1507.9	24.659	1.2128	.4449	873	0.00102	.754	192.7	0.865	.627	94.7
1.60	187.50	2501	1462.5	24.659	1.2138	.4431	858	0.00101	.900	187.5	0.710	.620	94.7
1.75	169.41	2452	1426.6	24.659	1.2143	.4415	843	0.00101	1.000	185.3	0.618	.685	102.5
2.00	150.00	2401	1386.5	24.659	1.2148	.4400	828	0.00100	1.103	187.0	0.526	.745	111.5
4.00	75.00	2112	1112.6	24.659	1.2230	.4295	757	0.00093	1.604	61.3	1.293	1.022	152.9
10.00	30.00	1773	925.6	24.659	1.2413	.4144	655	0.00085	2.155	22.1	2.193	1.265	189.3
20.00	15.00	1546	873.0	24.659	1.2502	.4025	594	0.00079	2.342	13.4	3.457	1.400	209.5
20.41	14.70	1540	874.5	24.659	1.2505	.4021	592	0.00079	2.356	13.57	3.505	1.403	210.0
40.00	7.50	1393	792.4	24.659	1.2585	.3898	536	0.00073	2.929	46.5	5.575	1.507	225.6
100.00	3.00	1107	706.2	24.659	1.2755	.3729	464	0.00066	3.446	28.4	10.691	1.619	242.4
200.00	1.50	950	648.9	24.659	1.2876	.3594	410	0.00060	3.853	26.7	17.627	1.687	252.5
400.00	.75	812	599.5	24.659	1.3009	.3483	360	0.00054	4.287	27.17	29.153	1.742	260.8
1000.00	.30	674	540.9	24.659	1.3182	.3337	300	0.00049	4.908	28.1	56.766	1.801	269.6
2000.00	.15	552	512.3	24.659	1.3311	.3229	250	0.00043	5.421	28.0	93.924	1.837	275.0
4000.00	.08	463	464.0	24.659	1.3432	.3135	211	0.00037	5.985	28.2	155.224	1.867	279.4

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(g) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P_e	Static pressure, P_c lb/in ² abs	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(K)	Viscosity, μ , micro poises	Thermal conductivity, k, cal/(sec)(K)(cm)	Mach number, M	Specific impulse in vacuum, I_{vac} , lb-sec/lb	Area ratio, A_e	Thrust coefficient, C_f	Specific impulse, I , lb-sec/lb
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	300.00	2372	1054.4	26.307	1.2311	0.4025	804	0.00040	0.000	0.000	0.000	0.000	0.0
1.05	285.71	2351	1045.7	26.307	1.2315	0.4018	799	0.00040	0.282	308.3	2.187	0.204	27.5
1.20	250.00	2292	1022.3	26.307	1.2328	0.4000	786	0.00039	0.549	195.4	1.269	0.392	52.9
1.40	214.29	2226	996.0	26.307	1.2343	0.3979	772	0.00038	0.750	173.9	1.066	0.529	71.3
1.60	187.50	2171	973.8	26.307	1.2357	0.3960	759	0.00037	0.892	168.9	1.011	0.621	85.7
1.79	167.18	2123	955.2	26.307	1.2369	0.3945	748	0.00037	1.000	168.0	1.000	0.689	92.9
2.00	150.00	2080	938.0	26.307	1.2380	0.3930	738	0.00036	1.094	168.0	1.008	0.747	100.6
4.00	75.00	1817	856.1	26.307	1.2450	0.3831	675	0.00032	1.598	181.2	1.288	1.023	137.8
10.00	30.00	1512	721.1	26.307	1.2570	0.3694	593	0.00028	2.155	199.5	2.165	1.263	170.3
20.00	15.00	1309	647.4	26.307	1.2669	0.3585	535	0.00024	2.549	211.1	3.393	1.396	188.2
20.41	14.70	1304	645.3	26.307	1.2672	0.3582	535	0.00024	2.560	211.4	3.439	1.400	188.7
40.00	7.50	1129	583.6	26.307	1.2777	0.3476	480	0.00021	2.940	220.7	5.440	1.502	202.4
100.00	3.00	921	512.9	26.307	1.2932	0.3332	411	0.00018	3.469	231.0	10.346	1.610	217.1
200.00	1.50	785	468.3	26.307	1.3061	0.3223	362	0.00015	3.890	237.3	16.952	1.675	225.8
400.00	0.75	666	430.4	26.307	1.3193	0.3121	316	0.00013	4.338	242.4	27.857	1.729	233.0
1000.00	0.30	531	389.1	26.307	1.3369	0.2998	261	0.00010	4.983	247.8	53.783	1.785	240.6
2000.00	0.15	445	363.6	26.307	1.3495	0.2917	224	0.00009	5.521	251.1	88.429	1.819	245.2
4000.00	0.08	371	342.4	26.307	1.3589	0.2860	190	0.00007	6.117	253.8	145.294	1.847	248.9
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	300.00	2069	855.0	27.313	1.2437	0.3713	742	0.00034	0.000	0.000	0.000	0.000	0.0
1.05	285.71	2020	847.7	27.313	1.2442	0.3707	737	0.00034	0.281	282.4	2.194	0.205	25.2
1.20	250.00	1996	828.0	27.313	1.2456	0.3690	724	0.00033	0.546	178.9	1.272	0.394	48.4
1.40	214.29	1936	806.0	27.313	1.2473	0.3670	710	0.00033	0.747	159.2	1.068	0.531	65.3
1.60	187.50	1866	787.4	27.313	1.2488	0.3652	697	0.00032	0.888	154.5	1.012	0.623	76.7
1.80	166.43	1841	771.2	27.313	1.2501	0.3636	686	0.00031	1.000	153.6	1.000	0.694	85.4
2.00	150.00	1803	757.5	27.313	1.2514	0.3622	677	0.00031	1.090	154.1	1.007	0.748	92.1
4.00	75.00	1566	672.6	27.313	1.2596	0.3530	614	0.00027	1.594	165.3	1.279	1.023	126.0
10.00	30.00	1292	577.6	27.313	1.2721	0.3402	536	0.00023	2.154	181.7	2.139	1.262	155.4
20.00	15.00	1112	517.0	27.313	1.2825	0.3303	481	0.00020	2.553	192.0	3.334	1.393	171.5
20.41	14.70	1107	515.4	27.313	1.2829	0.3300	479	0.00020	2.564	192.3	3.380	1.397	171.9
40.00	7.50	952	465.1	27.313	1.2939	0.3203	429	0.00018	2.950	200.5	5.317	1.496	184.2
100.00	3.00	770	407.9	27.313	1.3109	0.3070	364	0.00014	3.491	209.6	10.036	1.603	197.2
200.00	1.50	651	372.1	27.313	1.3239	0.2974	319	0.00012	3.923	215.0	16.345	1.665	205.0
400.00	0.75	548	341.9	27.313	1.3375	0.2883	277	0.00011	4.385	219.5	26.695	1.717	211.3
1000.00	0.30	433	309.3	27.313	1.3545	0.2780	227	0.00008	5.056	224.2	51.130	1.770	217.9
2000.00	0.15	361	289.4	27.313	1.3639	0.2727	193	0.00007	5.622	227.0	83.618	1.802	221.8
4000.00	0.08	299	272.8	27.313	1.3702	0.2693	163	0.00006	6.246	229.3	136.832	1.829	225.1

R = 4.000

R = 5.000

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P_c/P	Static pressure, P , lb./sq. in. abs.	Temperature, T , °K	Enthalpy, h , cal/g.	Molecular weight, M	Isentropic exponent, γ	Specific heat, c_p , cal/(g)(°K)	Viscosity, μ , micro poises	Thermal conductivity, k , cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I_{sp} , (lb)(sec)/lb.	Area ratio, g	Thrust coefficient, C_f	Specific impulse, I , (lb)(sec)/lb.
R = 0.150, PERCENT FUEL = 45.65, C/F = 1.190													
1.00	600.00	1183	5313.5	4.416	1.3396	1.7753	314	0.00073	0.000			0.000	0.0
1.05	571.43	1168	5287.7	4.416	1.3406	1.7710	311	0.00073	0.271	530.0	2.250	0.210	47.4
1.20	500.00	1129	5218.6	4.416	1.3436	1.7597	303	0.00070	0.527	334.2	1.297	0.403	90.8
1.40	428.57	1085	5141.8	4.416	1.3469	1.7472	293	0.00068	0.722	296.1	1.081	0.543	124.2
1.60	375.00	1049	5077.7	4.416	1.3497	1.7369	285	0.00066	0.860	266.6	1.018	0.636	143.2
1.87	321.68	1008	5006.8	4.416	1.3528	1.7257	276	0.00063	1.000	244.1	1.000	0.725	163.4
2.00	300.00	989	4975.4	4.416	1.3540	1.7210	272	0.00062	1.059	244.4	1.003	0.761	171.5
4.00	150.00	824	4693.4	4.416	1.3651	1.6825	234	0.0052	1.566	301.7	1.233	1.031	232.3
10.00	60.00	643	4392.5	4.416	1.3748	1.6505	188	0.0042	2.152	327.5	1.974	1.257	283.1
20.00	30.00	532	4209.8	4.416	1.3799	1.6344	159	0.0035	2.586	343.5	2.982	1.376	309.9
40.00	15.00	439	4058.9	4.416	1.3824	1.6268	133	0.0029	3.031	356.4	4.620	1.467	330.4
40.83	14.70	437	4054.8	4.416	1.3825	1.6266	132	0.0029	3.044	356.8	4.602	1.469	330.9
100.00	6.00	340	3899.0	4.416	1.3882	1.6093	104	0.0023	3.648	369.8	8.432	1.558	350.8
200.00	3.00	280	3802.6	4.416	1.3926	1.5961	85	0.0018	4.149	377.7	13.431	1.610	362.6
400.00	1.50	230	3723.2	4.416	1.4068	1.5562	70	0.0015	4.675	384.1	21.488	1.652	372.0
1000.00	.60	175	3640.1	4.416	1.4349	1.4847	55	0.0011	5.438	390.6	39.928	1.694	381.6
2000.00	.30	142	3590.9	4.416	1.4550	1.4389	45	0.0009	6.096	394.3	63.572	1.719	387.2
4000.00	.15	114	3551.2	4.416	1.4705	1.4065	36	0.0007	6.845	397.3	100.938	1.739	391.6
R = 0.200, PERCENT FUEL = 38.65, C/F = 1.587													
1.00	600.00	1514	2969.7	5.216	1.3079	1.6183	422	0.00084	0.000			0.000	0.0
1.05	571.43	1497	2941.7	5.216	1.3090	1.6140	399	0.00083	0.274	552.2	2.253	0.209	49.3
1.20	500.00	1450	2866.8	5.216	1.3120	1.6022	389	0.00081	0.533	348.6	1.289	0.400	94.6
1.40	428.57	1398	2783.1	5.216	1.3155	1.5887	378	0.00078	0.730	309.3	1.077	0.539	127.4
1.60	375.00	1354	2713.2	5.216	1.3185	1.5772	369	0.00076	0.869	299.6	1.016	0.632	146.4
1.87	324.94	1307	2640.5	5.216	1.3217	1.5651	359	0.00073	1.000	297.3	1.000	0.716	169.2
2.00	300.00	1282	2601.1	5.216	1.3236	1.5584	353	0.00072	1.068	297.8	1.004	0.757	179.1
4.00	150.00	1079	2290.0	5.216	1.3391	1.5046	307	0.0061	1.572	316.7	1.244	1.029	243.2
10.00	60.00	852	1954.3	5.216	1.3558	1.4516	251	0.0048	2.148	344.7	2.009	1.257	297.2
20.00	30.00	709	1748.8	5.216	1.3656	1.4232	213	0.0040	2.573	362.0	3.049	1.379	325.9
40.00	15.00	588	1578.0	5.216	1.3715	1.4066	179	0.0034	3.010	376.0	4.739	1.472	348.0
40.83	14.70	585	1573.4	5.216	1.3716	1.4062	178	0.0034	3.023	376.4	4.802	1.474	348.6
100.00	6.00	458	1396.3	5.216	1.3771	1.3913	142	0.0026	3.619	390.5	8.679	1.565	370.0
200.00	3.00	379	1286.2	5.216	1.3811	1.3807	117	0.0022	4.111	399.1	13.070	1.619	382.7
400.00	1.50	312	1195.2	5.216	1.3861	1.3677	96	0.0018	4.638	406.1	22.296	1.662	392.9
1000.00	.60	242	1099.0	5.216	1.3973	1.3400	74	0.0013	5.394	413.4	41.979	1.706	403.5
2000.00	.30	198	1041.1	5.216	1.4126	1.2977	61	0.0011	6.014	417.7	67.687	1.733	409.7
4000.00	.15	161	993.9	5.216	1.4390	1.2568	50	0.0009	6.704	421.1	108.754	1.754	414.6
R = 0.250, PERCENT FUEL = 33.51, C/F = 1.984													
1.00	600.00	1817	1249.3	6.016	1.2835	1.4955	481	0.00092	0.000			0.000	0.0
1.05	571.43	1797	1220.2	6.016	1.2844	1.4917	477	0.00091	0.276	563.4	2.219	0.207	50.3
1.20	500.00	1745	1142.1	6.016	1.2870	1.4813	467	0.00089	0.538	356.2	1.283	0.398	96.6
1.40	428.57	1686	1054.7	6.016	1.2900	1.4694	456	0.00086	0.736	316.3	1.073	0.536	130.1
1.60	375.00	1636	981.5	6.016	1.2926	1.4591	446	0.00083	0.876	306.6	1.015	0.629	152.7
1.87	327.79	1586	909.9	6.016	1.2954	1.4485	436	0.00081	1.000	304.5	1.000	0.708	171.8
2.00	300.00	1555	864.0	6.016	1.2973	1.4415	429	0.00080	1.076	305.1	1.005	0.754	183.1
4.00	150.00	1322	535.2	6.016	1.3125	1.3873	378	0.0068	1.579	325.5	1.256	1.027	249.3
10.00	60.00	1057	176.3	6.016	1.3329	1.3225	314	0.0054	2.147	355.3	2.048	1.258	305.6
20.00	30.00	887	995.4	6.016	1.3461	1.2848	269	0.0046	2.563	373.7	3.127	1.382	335.7
40.00	15.00	740	976.3	6.016	1.3509	1.2559	228	0.0038	2.987	386.6	4.883	1.478	359.0
40.83	14.70	736	9763.3	6.016	1.3512	1.2551	227	0.0038	3.000	389.0	4.949	1.481	359.6
100.00	6.00	580	9569.3	6.016	1.3663	1.2320	181	0.0030	3.581	404.2	8.985	1.575	382.3
200.00	3.00	481	9448.1	6.016	1.3717	1.2191	151	0.0025	4.064	413.4	14.395	1.630	395.9
400.00	1.50	399	9347.6	6.016	1.3755	1.2100	124	0.0020	4.582	420.9	23.207	1.675	406.8
1000.00	.60	310	9240.9	6.016	1.3821	1.1948	95	0.0015	5.327	428.7	43.891	1.722	418.0
2000.00	.30	256	9176.3	6.016	1.3885	1.1805	78	0.0012	5.945	433.4	71.275	1.749	424.7
4000.00	.15	210	9123.1	6.016	1.4039	1.1482	64	0.0010	6.606	437.1	115.642	1.771	430.1
R = 0.300, PERCENT FUEL = 29.57, C/F = 2.381													
1.00	600.00	2094	9932.7	6.815	1.2647	1.3934	551	0.00097	0.000			0.000	0.0
1.05	571.43	2073	9903.1	6.815	1.2654	1.3904	547	0.00096	0.278	568.6	2.208	0.206	50.8
1.20	500.00	2015	9823.5	6.815	1.2675	1.3817	537	0.00094	0.542	359.8	1.278	0.396	97.5
1.40	428.57	1951	9734.4	6.815	1.2701	1.3716	525	0.00091	0.741	319.8	1.071	0.533	131.4
1.60	375.00	1896	9659.5	6.815	1.2724	1.3622	515	0.00089	0.881	310.2	1.013	0.626	154.2
1.87	330.09	1845	9589.9	6.815	1.2746	1.3534	505	0.00087	1.000	308.2	1.000	0.701	172.7
2.00	300.00	1807	9539.0	6.815	1.2764	1.3467	498	0.00085	1.082	309.0	1.006	0.751	185.1
4.00	150.00	1551	9200.2	6.815	1.2898	1.2980	444	0.0074	1.585	330.4	1.266	1.025	252.5
10.00	60.00	1256	8826.3	6.815	1.3097	1.2332	375	0.0060	2.148	361.6	2.084	1.260	310.3
20.00	30.00	1062	8592.4	6.815	1.3220	1.1888	325	0.0050	2.555	381.0	3.205	1.387	341.5
40.00	15.00	894	8395.1	6.815	1.3365	1.1529	278	0.0042	2.969	396.8	5.035	1.485	368.8
40.83	14.70	889	8389.8	6.815	1.3369	1.1520	277	0.0042	2.981	397.2	5.104	1.488	368.4
100.00	6.00	706	8182.2	6.815	1.3532	1.1173	225	0.0033	3.544	413.2	9.321	1.585	390.3
200.00	3.00	589	8051.7	6.815	1.3605	1.1006	187	0.0027	4.014	423.0	14.986	1.643	404.6
400.00	1.50	489	7943.1	6.815	1.3667	1.0868	156	0.0023	4.518	431.0	24.223	1.689	416.1
1000.00	.60	382	7827.2	6.815	1.3725	1.0745	120	0.0017	5.248	439.4	45.476	1.738	428.0
2000.00	.30	316	7756.9	6.815	1.3775	1.0640	98	0.0014	5.853	444.3	74.873	1.767	435.1
4000.00	.15	261	7698.7	6.815	1.3829	1.0531	80	0.0011	6.511	448.4	122.117	1.790	440.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P	Static pressure, P, lb/in. abs.	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , lb(sec)/lb	Area ratio, A	Thrust coefficient, C _F	Specific impulse, I, lb(sec)/lb
R = 0.350, PERCENT FUEL = 26.47, O/F = 2.778													
1.00	600.00	2347	8892.8	7.610	1.2500	1.3056	611	0.00100	0.000	569.9	2.199	0.000	0.0
1.05	571.43	2324	8863.0	7.610	1.2507	1.3029	607	0.00199	.280	569.9	2.199	.205	50.9
1.20	500.00	2263	8783.0	7.610	1.2525	1.2955	597	0.00097	.545	360.8	1.274	.394	97.7
1.40	428.57	2193	8693.3	7.610	1.2546	1.2868	585	0.00094	.745	320.9	1.069	.532	131.7
1.60	375.00	2135	8617.9	7.610	1.2565	1.2793	575	0.00092	.886	311.5	1.012	.624	154.7
1.81	331.93	2082	8550.7	7.610	1.2582	1.2724	566	0.00090	1.000	309.6	1.000	.696	172.5
2.00	300.00	2039	8496.3	7.610	1.2597	1.2665	558	0.00089	1.087	310.5	1.007	.749	185.7
4.00	150.00	1763	8152.6	7.610	1.2714	1.2233	504	0.00078	1.590	332.7	1.274	1.024	253.8
10.00	60.00	1443	7770.0	7.610	1.2893	1.1638	432	0.00064	2.150	365.0	2.116	1.261	312.6
20.00	30.00	1231	7528.4	7.610	1.3043	1.1192	379	0.00055	2.551	385.2	3.276	1.390	344.6
40.00	15.00	1044	7322.8	7.610	1.3196	1.0783	328	0.00046	2.954	401.7	5.180	1.491	369.6
40.83	14.70	1039	7317.2	7.610	1.3200	1.0772	326	0.00046	2.966	402.1	5.252	1.494	370.3
100.00	6.00	842	7099.0	7.610	1.3371	1.0358	266	0.00036	3.513	419.0	9.659	1.594	395.1
200.00	3.00	697	6960.9	7.610	1.3480	1.0115	224	0.00030	3.967	429.3	15.596	1.654	410.0
400.00	1.50	582	6842.4	7.610	1.3528	.9950	187	0.00025	4.457	437.8	25.296	1.703	422.1
1000.00	.60	457	6721.6	7.610	1.3638	.9790	147	0.00019	5.166	446.6	48.178	1.754	434.6
2000.00	.30	379	6646.1	7.610	1.3688	.9693	120	0.00016	5.756	451.9	78.663	1.784	442.1
4000.00	.15	314	6583.5	7.610	1.3738	.9597	97	0.00013	6.399	456.2	128.622	1.809	448.3
R = 0.400, PERCENT FUEL = 23.95, O/F = 3.175													
1.00	600.00	2574	8050.5	8.396	1.2385	1.2292	663	0.00101	0.000	568.3	2.191	0.000	0.0
1.05	571.43	2550	8020.9	8.396	1.2390	1.2271	659	0.00100	.281	568.3	2.191	.205	50.7
1.20	500.00	2485	7941.4	8.396	1.2405	1.2210	649	0.00098	.547	360.0	1.271	.393	97.5
1.40	428.57	2412	7852.0	8.396	1.2423	1.2137	638	0.00096	.748	320.4	1.067	.530	131.4
1.60	375.00	2350	7776.8	8.396	1.2439	1.2071	627	0.00094	.890	311.1	1.012	.622	154.3
1.80	333.33	2296	7712.1	8.396	1.2454	1.2012	618	0.00093	1.000	309.4	1.000	.692	171.6
2.00	300.00	2249	7655.4	8.396	1.2468	1.1958	610	0.00091	1.091	310.3	1.007	.748	185.4
4.00	150.00	1956	7310.9	8.396	1.2586	1.1592	557	0.00081	1.595	333.1	1.281	1.023	253.7
10.00	60.00	1615	6924.5	8.396	1.2724	1.1057	484	0.00068	2.152	366.2	2.143	1.262	313.0
20.00	30.00	1388	6678.4	8.396	1.2803	1.0634	429	0.00058	2.548	386.9	3.338	1.393	345.5
40.00	15.00	1186	6467.6	8.396	1.3013	1.0222	375	0.00049	2.944	404.0	5.310	1.497	371.1
40.83	14.70	1181	6461.8	8.396	1.3018	1.0211	374	0.00049	2.955	404.5	5.384	1.499	371.8
100.00	6.00	954	6236.1	8.396	1.3108	.9745	308	0.00039	3.487	422.1	9.975	1.602	397.3
200.00	3.00	804	6092.2	8.396	1.3337	.9460	261	0.00032	3.927	432.9	16.185	1.665	412.8
400.00	1.50	675	5971.1	8.396	1.3443	.9241	220	0.00027	4.401	441.7	26.355	1.715	425.4
1000.00	.60	532	5840.7	8.396	1.3551	.9033	173	0.00021	5.088	451.0	50.405	1.768	438.5
2000.00	.30	443	5760.9	8.396	1.3607	.8928	143	0.00017	5.663	456.6	82.493	1.800	446.3
4000.00	.15	369	5694.5	8.396	1.3661	.8833	117	0.00014	6.288	461.2	135.208	1.826	452.8
R = 0.450, PERCENT FUEL = 21.87, O/F = 3.571													
1.00	600.00	2773	7354.5	9.167	1.2292	1.1624	707	0.00101	0.000	564.6	2.186	0.000	0.0
1.05	571.43	2748	7325.3	9.167	1.2297	1.1604	704	0.00101	.282	564.6	2.186	.204	50.4
1.20	500.00	2680	7246.7	9.167	1.2311	1.1550	694	0.00099	.549	357.9	1.268	.392	96.8
1.40	428.57	2604	7158.4	9.167	1.2326	1.1487	682	0.00097	.751	318.6	1.066	.529	130.6
1.60	375.00	2539	7084.0	9.167	1.2339	1.1433	672	0.00095	.893	309.5	1.011	.621	153.4
1.79	334.56	2484	7021.9	9.167	1.2352	1.1386	663	0.00094	1.000	307.8	1.000	.689	170.1
2.00	300.00	2433	6963.8	9.167	1.2364	1.1338	655	0.00092	1.095	308.8	1.008	.746	184.4
4.00	150.00	2127	6621.6	9.167	1.2490	1.1016	602	0.00083	1.598	332.0	1.286	1.022	252.5
10.00	60.00	1769	6235.4	9.167	1.2589	1.0541	529	0.00070	2.153	365.5	2.165	1.263	312.0
20.00	30.00	1530	5987.8	9.167	1.2713	1.0157	474	0.00061	2.546	386.7	3.389	1.396	344.8
40.00	15.00	1316	5774.3	9.167	1.2855	.9761	418	0.00052	2.936	404.3	5.420	1.501	370.8
40.83	14.70	1310	5768.5	9.167	1.2859	.9750	417	0.00052	2.947	404.7	5.497	1.504	371.5
100.00	6.00	1068	5538.2	9.167	1.3033	.9267	348	0.00042	3.467	422.9	10.256	1.609	397.5
200.00	3.00	905	5390.3	9.167	1.3195	.8952	298	0.00035	3.895	434.1	16.723	1.674	413.4
400.00	1.50	763	5265.1	9.167	1.3322	.8693	252	0.00029	4.353	443.3	27.347	1.726	426.4
1000.00	.60	605	5129.7	9.167	1.3452	.8448	199	0.00022	5.021	453.0	52.536	1.781	440.0
2000.00	.30	506	5046.4	9.167	1.3533	.8303	165	0.00018	5.577	458.8	86.213	1.814	448.1
4000.00	.15	422	4976.9	9.167	1.3569	.8207	136	0.00015	6.187	463.6	141.612	1.841	454.8
R = 0.500, PERCENT FUEL = 20.12, O/F = 3.968													
1.00	600.00	2944	6769.6	9.919	1.2218	1.1037	745	0.00101	0.000	559.4	2.181	0.000	0.0
1.05	571.43	2918	6741.0	9.919	1.2222	1.1020	741	0.00100	.283	559.4	2.181	.204	49.9
1.20	500.00	2846	6663.8	9.919	1.2234	1.0971	731	0.00099	.551	354.7	1.266	.391	95.9
1.40	428.57	2769	6577.1	9.919	1.2248	1.0914	720	0.00097	.753	315.9	1.065	.528	129.4
1.60	375.00	2702	6503.9	9.919	1.2261	1.0865	710	0.00095	.895	306.9	1.011	.620	152.0
1.79	335.48	2647	6444.3	9.919	1.2272	1.0823	701	0.00093	1.000	305.4	1.000	.686	168.3
2.00	300.00	2592	6385.6	9.919	1.2282	1.0781	693	0.00092	1.097	306.4	1.008	.745	182.8
4.00	150.00	2275	6048.0	9.919	1.2398	1.0500	640	0.00083	1.601	329.7	1.291	1.022	250.6
10.00	60.00	1904	5665.2	9.919	1.2480	1.0081	568	0.00072	2.154	363.5	2.183	1.264	310.0
20.00	30.00	1655	5418.4	9.919	1.2599	.9730	513	0.00063	2.544	385.0	3.431	1.398	342.9
40.00	15.00	1431	5204.5	9.919	1.2724	.9359	457	0.00054	2.930	402.8	5.512	1.505	369.0
40.83	14.70	1424	5198.6	9.919	1.2728	.9348	455	0.00054	2.941	403.3	5.591	1.508	369.7
100.00	6.00	1170	4966.4	9.919	1.2916	.8875	383	0.00044	3.452	421.9	10.495	1.615	396.1
200.00	3.00	997	4816.2	9.919	1.3065	.8539	331	0.00037	3.869	434.4	17.193	1.681	412.3
400.00	1.50	845	4688.5	9.919	1.3202	.8260	282	0.00030	4.315	442.9	28.235	1.735	425.5
1000.00	.60	674	4549.6	9.919	1.3357	.7971	225	0.00024	4.962	452.9	54.491	1.792	439.5
2000.00	.30	565	4463.8	9.919	1.3449	.7812	187	0.00019	5.504	458.9	89.675	1.827	447.9
4000.00	.15	472	4391.9	9.919	1.3524	.7688	155	0.00016	6.096	463.9	147.626	1.855	454.9

TABLE II. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P/P ₀	Static pressure, P, lb/sq in abs	Temperature, T, K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/g (°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/sec (°K cm)	Mach number M	Specific impulse in vacuum, I _{sp} , lb-sec/lb	Area ratio, E	Thrust coefficient, C _f	Specific impulse, I _{sp} , lb-sec/lb
R = 0.600, PERCENT FUEL = 17.35, O/F = 4.762													
1.00	630.00	3208	5841.5	11.347	1.2112	1.0094	803	0.00038	0.000	0.000		0.000	0.0
1.05	571.43	3180	5614.3	11.347	1.2115	1.0091	800	0.00036	0.284	246.0	2.175	1.203	48.7
1.20	500.00	3107	5740.3	11.347	1.2120	0.9994	790	0.00036	0.553	346.4	1.263	0.990	93.7
1.40	428.57	3024	5658.1	11.347	1.2130	0.9920	778	0.00034	0.756	308.7	1.005	0.720	126.4
1.60	375.00	2954	5285.2	11.347	1.2146	0.9910	768	0.00033	0.898	300.0	1.020	0.619	148.5
1.78	336.81	2893	5053.1	11.347	1.2155	0.9877	760	0.00032	1.000	298.0	1.000	0.682	163.6
2.00	300.00	2839	4775.0	11.347	1.2169	0.9841	752	0.00030	1.101	299.7	1.009	0.744	178.6
4.00	150.00	2508	3190.2	11.347	1.2227	0.9516	700	0.00033	1.804	323.0	1.298	1.021	245.1
10.00	60.00	2119	4780.9	11.347	1.2328	0.9274	629	0.00032	2.156	356.8	2.209	1.265	303.8
20.00	30.00	1851	4340.3	11.347	1.2442	0.8987	574	0.00034	2.544	376.4	3.492	1.401	336.5
40.00	15.00	1613	4350.4	11.347	1.2553	0.8666	518	0.00036	2.922	396.5	5.648	1.910	362.6
40.83	14.70	1607	4324.7	11.347	1.2536	0.8558	518	0.00036	2.933	397.0	5.730	1.913	362.3
100.00	6.00	1334	4094.4	11.347	1.2703	0.8224	443	0.00036	3.431	416.0	10.859	1.824	369.9
200.00	3.00	1148	3944.0	11.347	1.2891	0.7899	387	0.00039	3.833	427.9	17.925	1.692	400.3
400.00	1.50	981	3813.0	11.347	1.2999	0.7590	334	0.00033	4.260	437.7	29.654	1.749	413.9
1000.00	0.60	790	3673.4	11.347	1.3161	0.7236	270	0.00025	4.876	446.2	57.761	1.807	434.4
2000.00	0.30	667	3585.1	11.347	1.3299	0.7060	227	0.00021	5.391	454.6	99.510	1.846	443.7
4000.00	0.15	560	3510.8	11.347	1.3397	0.6908	189	0.00017	5.955	459.8	157.952	1.876	450.3
R = 0.700, PERCENT FUEL = 15.25, O/F = 5.556													
1.00	600.00	3381	5138.3	12.684	1.2044	0.9245	846	0.00035	0.000	0.000		0.000	0.0
1.05	571.43	3353	5112.3	12.684	1.2047	0.9234	842	0.00034	0.285	230.7	2.171	1.203	47.4
1.20	500.00	3278	5043.0	12.684	1.2058	0.9201	832	0.00033	0.554	330.0	1.263	0.989	91.0
1.40	428.57	3192	4780.8	12.684	1.2066	0.9164	820	0.00031	0.756	300.0	1.005	0.923	126.4
1.60	375.00	3120	4498.7	12.684	1.2079	0.9132	810	0.00030	0.900	291.9	1.009	0.819	148.4
1.78	337.67	3064	4247.8	12.684	1.2082	0.9106	802	0.00029	1.000	290.8	1.000	0.880	159.0
2.00	300.00	3002	4791.3	12.684	1.2090	0.9076	793	0.00028	1.103	291.7	1.009	0.943	173.7
4.00	150.00	2660	4433.9	12.684	1.2146	0.8922	742	0.00030	1.807	314.7	1.902	1.021	245.6
10.00	60.00	2257	4131.1	12.684	1.2233	0.8729	672	0.00031	2.157	349.1	2.220	1.266	296.0
20.00	30.00	1985	3900.7	12.684	1.2314	0.8549	617	0.00034	2.541	369.4	3.532	1.403	326.2
40.00	15.00	1738	3896.4	12.684	1.2413	0.8271	561	0.00036	2.918	387.7	5.737	1.914	352.0
40.83	14.70	1732	3892.8	12.684	1.2416	0.8063	559	0.00036	2.927	388.0	5.821	1.917	352.6
100.00	6.00	1448	3469.8	12.684	1.2566	0.7679	486	0.00037	3.418	407.0	11.000	1.858	381.0
200.00	3.00	1253	3323.0	12.684	1.2704	0.7512	429	0.00040	3.812	419.0	18.418	1.700	397.4
400.00	1.50	1078	3196.4	12.684	1.2851	0.7073	373	0.00034	4.226	429.0	30.835	1.758	411.1
1000.00	0.60	875	3056.3	12.684	1.3033	0.6726	305	0.00027	4.822	439.7	60.039	1.820	425.0
2000.00	0.30	742	2988.5	12.684	1.3177	0.6506	258	0.00022	5.317	446.2	99.783	1.858	434.5
4000.00	0.15	627	2894.2	12.684	1.3291	0.6357	217	0.00018	5.860	452.6	162.847	1.890	441.9
R = 0.800, PERCENT FUEL = 13.60, O/F = 6.349													
1.00	600.00	3481	4586.9	13.859	1.2004	0.8591	875	0.00031	0.000	0.000		0.000	0.0
1.05	571.43	3453	4562.6	13.859	1.2008	0.8580	872	0.00030	0.286	214.8	2.166	1.202	45.9
1.20	500.00	3376	4497.2	13.859	1.2019	0.8522	861	0.00029	0.555	320.0	1.260	0.989	89.5
1.40	428.57	3290	4423.6	13.859	1.2024	0.8489	851	0.00028	0.759	291.4	1.002	0.923	119.2
1.60	375.00	3217	4261.3	13.859	1.2032	0.8490	839	0.00026	0.902	283.5	1.009	0.817	140.1
1.78	337.67	3161	4314.0	13.859	1.2039	0.8466	831	0.00025	1.000	282.1	1.000	0.879	154.1
2.00	300.00	3098	4296.3	13.859	1.2046	0.8442	822	0.00024	1.103	283.2	1.010	0.942	168.6
4.00	150.00	2750	3969.9	13.859	1.2097	0.8273	770	0.00028	1.808	309.7	1.904	1.020	231.7
10.00	60.00	2341	3636.1	13.859	1.2177	0.8022	700	0.00029	2.157	338.4	2.236	1.267	287.6
20.00	30.00	2069	3417.4	13.859	1.2254	0.7803	646	0.00032	2.540	359.4	3.556	1.405	319.0
40.00	15.00	1814	3224.8	13.859	1.2342	0.7527	590	0.00035	2.913	377.1	5.791	1.916	344.9
40.83	14.70	1807	3219.3	13.859	1.2345	0.7349	588	0.00035	2.924	377.6	5.876	1.919	344.9
100.00	6.00	1518	3058.4	13.859	1.2485	0.7203	514	0.00036	3.410	396.4	11.047	1.833	370.8
200.00	3.00	1319	2863.5	13.859	1.2625	0.6960	457	0.00040	3.799	406.3	18.724	1.704	387.0
400.00	1.50	1139	2743.6	13.859	1.2776	0.6596	401	0.00034	4.207	416.2	31.251	1.764	400.5
1000.00	0.60	929	2603.0	13.859	1.2991	0.6294	330	0.00027	4.789	426.9	61.924	1.827	415.0
2000.00	0.30	791	2522.7	13.859	1.3091	0.6073	282	0.00022	5.272	439.5	102.879	1.860	423.6
4000.00	0.15	670	2450.2	13.859	1.3216	0.5923	237	0.00018	5.801	449.9	170.764	1.899	431.2
R = 0.900, PERCENT FUEL = 12.28, O/F = 7.143													
1.00	600.00	3526	4142.9	14.930	1.1982	0.8047	896	0.00027	0.000	0.000		0.000	0.0
1.05	571.43	3498	4120.1	14.930	1.1985	0.8036	892	0.00026	0.286	214.8	2.167	1.202	45.9
1.20	500.00	3421	4056.7	14.930	1.1992	0.8003	881	0.00025	0.555	317.0	1.260	0.989	89.6
1.40	428.57	3334	3987.4	14.930	1.2001	0.7963	869	0.00024	0.759	288.0	1.001	0.923	119.6
1.60	375.00	3261	3930.8	14.930	1.2009	0.7926	857	0.00023	0.902	279.0	1.007	0.817	140.7
1.78	337.67	3200	3886.6	14.930	1.2015	0.7936	851	0.00022	1.000	278.0	1.000	0.879	154.2
2.00	300.00	3141	3835.7	14.930	1.2022	0.7913	842	0.00021	1.103	278.8	1.010	0.942	168.6
4.00	150.00	2792	3562.3	14.930	1.2070	0.7760	789	0.00025	1.809	296.7	1.906	1.020	244.8
10.00	60.00	2381	3247.3	14.930	1.2145	0.7533	719	0.00026	2.157	326.9	2.241	1.267	279.2
20.00	30.00	2103	3040.7	14.930	1.2218	0.7311	664	0.00030	2.539	349.0	3.569	1.406	309.7
40.00	15.00	1851	2858.5	14.930	1.2304	0.7109	606	0.00033	2.911	366.4	5.820	1.917	334.3
40.83	14.70	1844	2853.5	14.930	1.2306	0.7102	606	0.00033	2.922	366.8	5.906	1.920	334.3
100.00	6.00	1553	2691.4	14.930	1.2441	0.6784	532	0.00034	3.406	389.2	11.028	1.832	360.3
200.00	3.00	1352	2517.6	14.930	1.2570	0.6479	475	0.00039	3.792	399.9	18.892	1.707	376.1
400.00	1.50	1170	2401.4	14.930	1.2703	0.6222	418	0.00033	4.196	409.7	31.251	1.767	389.3
1000.00	0.60	957	2272.0	14.930	1.2897	0.5916	347	0.00026	4.772	417.2	62.099	1.834	401.5
2000.00	0.30	817	2190.3	14.930	1.3029	0.5711	297	0.00021	5.248	423.7	104.470	1.871	412.7
4000.00	0.15	693	2126.8	14.930	1.3159	0.5531	251	0.00017	5.769	429.0	173.717	1.904	421.2

TABLE II. - Concluded. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute; Frozen composition during isentropic expansion

Pressure ratio, P/P	Static pressure, P _s , lb/in ² abs	Temp., T, K	Enthalpy, h, cal/g	Molecular weight, \bar{M}	Isentropic exponent, γ	Specific heat, c_p , cal/g ⁰ K ¹	Viscosity, μ , micropoises	Thermal conductivity, k , cal/sec ⁰ K/cm	Mach number, M	Specific impulse in vacuum, I _{sp} , lb-sec/lb	Area ratio, E	Thrust coefficient, C _F	Specific impulse, I _{sp} , lb-sec/lb
R = 1.000, PERCENT FUEL = 11.19, O/F = 7.937													
1.00	600.00	3534	3777.9	15.886	1.1972	0.7592	910	0.00083	0.000	484.5	2.166	0.000	0.0
1.05	571.43	3503	3756.4	15.886	1.1975	.7584	906	.00083	.286	484.5	2.166	.202	43.2
1.20	500.00	3429	3698.5	15.886	1.1982	.7560	895	.00082	.556	484.5	2.166	.389	89.1
1.40	428.57	3342	3633.2	15.886	1.1991	.7533	882	.00080	.760	484.5	2.166	.525	114.2
1.60	375.00	3269	3578.0	15.886	1.1999	.7508	872	.00079	.903	484.5	2.166	.617	131.9
1.77	338.23	3214	3536.6	15.886	1.2005	.7489	864	.00078	1.000	484.5	2.166	.677	144.9
2.00	300.00	3149	3488.4	15.886	1.2012	.7468	854	.00077	1.100	484.5	2.166	.742	158.7
4.00	150.00	2801	3230.7	15.886	1.2099	.7327	801	.00071	1.609	484.5	2.166	1.020	218.2
10.00	60.00	2390	2935.7	15.886	1.2135	.7115	730	.00065	2.157	484.5	2.244	1.267	271.0
20.00	30.00	2112	2738.7	15.886	1.2204	.6927	674	.00057	2.939	484.5	3.275	1.406	300.7
40.00	15.00	1861	2566.6	15.886	1.2297	.6720	618	.00051	2.911	484.5	5.835	1.518	324.6
40.83	14.70	1853	2561.9	15.886	1.2290	.6714	616	.00051	2.922	484.5	5.919	1.521	325.3
100.00	6.00	1563	2370.8	15.886	1.2421	.6416	542	.00043	3.404	484.5	11.363	1.636	349.9
200.00	3.00	1362	2244.2	15.886	1.2543	.6169	484	.00037	3.789	484.5	18.966	1.708	362.3
400.00	1.50	1160	2134.2	15.886	1.2676	.5921	428	.00032	4.192	484.5	31.744	1.768	376.2
1000.00	.60	967	2011.5	15.886	1.2870	.5609	356	.00026	4.764	484.5	62.740	1.833	392.0
2000.00	.30	826	1933.9	15.886	1.3013	.5403	306	.00021	5.238	411.8	104.909	1.873	400.6
4000.00	.15	701	1867.6	15.886	1.3149	.5226	260	.00018	5.755	417.0	175.109	1.906	407.7
R = 1.500, PERCENT FUEL = 7.749, O/F = 11.905													
1.00	600.00	3374	2626.1	19.463	1.1996	0.6136	930	0.00069	0.000	427.7	2.166	0.000	0.0
1.05	571.43	3346	2609.3	19.463	1.1999	.6129	925	.00069	.286	427.7	2.166	.202	38.2
1.20	500.00	3273	2564.2	19.463	1.2007	.6109	914	.00067	.555	427.7	2.166	.389	73.4
1.40	428.57	3189	2513.4	19.463	1.2016	.6086	901	.00066	.759	427.7	2.166	.525	99.0
1.60	375.00	3118	2470.4	19.463	1.2023	.6067	889	.00065	.902	427.7	2.166	.617	116.4
1.77	338.23	3065	2437.8	19.463	1.2030	.6051	881	.00065	1.000	427.7	2.166	.678	128.0
2.00	300.00	3003	2400.6	19.463	1.2037	.6032	871	.00064	1.105	427.7	2.166	.742	140.1
4.00	150.00	2668	2200.2	19.463	1.2088	.5912	813	.00058	1.609	427.7	3.105	1.020	192.5
10.00	60.00	2272	1969.5	19.463	1.2166	.5735	737	.00052	2.157	427.7	4.238	1.267	239.0
20.00	30.00	2003	1816.3	19.463	1.2238	.5584	679	.00047	2.939	427.7	5.861	1.406	265.1
40.00	15.00	1765	1685.2	19.463	1.2329	.5413	620	.00042	2.911	427.7	10.406	1.518	286.1
40.83	14.70	1756	1681.5	19.463	1.2327	.5406	619	.00041	2.924	427.7	10.487	1.519	286.7
100.00	6.00	1477	1533.9	19.463	1.2440	.5172	543	.00035	3.409	427.7	18.966	1.636	308.3
200.00	3.00	1285	1436.3	19.463	1.2579	.4979	486	.00030	3.797	427.7	31.744	1.708	321.8
400.00	1.50	1112	1351.6	19.463	1.2711	.4787	430	.00026	4.203	427.7	52.740	1.768	333.0
1000.00	.60	909	1257.3	19.463	1.2895	.4548	360	.00021	4.781	427.7	104.909	1.833	345.1
2000.00	.30	776	1197.7	19.463	1.3032	.4385	311	.00018	5.238	427.7	175.109	1.873	352.5
4000.00	.15	659	1147.0	19.463	1.3160	.4252	266	.00015	5.780	427.7	286.498	1.901	358.7
R = 2.000, PERCENT FUEL = 5.927, O/F = 15.873													
1.00	600.00	3158	2016.0	21.832	1.2049	0.5352	919	0.00060	0.000	390.6	2.171	0.000	0.0
1.05	571.43	3132	2001.1	21.832	1.2052	.5346	910	.00059	.285	390.6	2.171	.203	34.9
1.20	500.00	3061	1959.6	21.832	1.2060	.5328	902	.00058	.554	390.6	2.171	.389	67.0
1.40	428.57	2981	1922.0	21.832	1.2071	.5309	890	.00057	.758	390.6	2.171	.525	90.4
1.60	375.00	2914	1885.2	21.832	1.2080	.5285	877	.00056	.900	390.6	2.171	.617	106.3
1.77	338.23	2861	1855.8	21.832	1.2088	.5270	868	.00056	1.000	390.6	2.171	.678	117.0
2.00	300.00	2804	1826.2	21.832	1.2095	.5252	858	.00055	1.105	390.6	2.171	.742	127.9
4.00	150.00	2483	1661.5	21.832	1.2151	.5143	797	.00050	1.609	390.6	3.102	1.021	175.6
10.00	60.00	2105	1470.5	21.832	1.2238	.4977	718	.00044	2.157	390.6	4.225	1.266	217.9
20.00	30.00	1892	1349.8	21.832	1.2316	.4840	658	.00039	2.941	390.6	5.850	1.403	241.5
40.00	15.00	1622	1235.4	21.832	1.2407	.4692	599	.00035	2.911	390.6	10.411	1.514	260.5
40.83	14.70	1616	1233.5	21.832	1.2409	.4685	597	.00035	2.924	390.6	10.487	1.517	261.0
100.00	6.00	1365	1112.6	21.832	1.2549	.4461	521	.00029	3.420	390.6	18.966	1.636	280.4
200.00	3.00	1172	1033.5	21.832	1.2699	.4321	463	.00025	3.814	390.6	31.744	1.708	292.5
400.00	1.50	1010	969.3	21.832	1.2800	.4161	411	.00022	4.228	390.6	52.740	1.768	304.5
1000.00	.60	822	866.1	21.832	1.2977	.3963	344	.00018	4.781	390.6	104.909	1.833	315.3
2000.00	.30	700	840.2	21.832	1.3100	.3835	298	.00015	5.238	390.6	175.109	1.873	319.9
4000.00	.15	592	799.5	21.832	1.3234	.3720	255	.00012	5.780	390.6	286.498	1.901	325.4
R = 3.000, PERCENT FUEL = 4.031, O/F = 23.810													
1.00	600.00	2747	1381.4	24.718	1.2174	0.4602	867	0.00048	0.000	342.5	2.179	0.000	0.0
1.05	571.43	2723	1370.7	24.718	1.2178	.4595	862	.00048	.284	342.5	2.179	.203	30.6
1.20	500.00	2659	1341.8	24.718	1.2189	.4577	852	.00047	.551	342.5	2.179	.391	58.7
1.40	428.57	2586	1309.3	24.718	1.2201	.4559	838	.00046	.754	342.5	2.179	.527	79.2
1.60	375.00	2524	1281.9	24.718	1.2216	.4545	825	.00045	.898	342.5	2.179	.619	93.1
1.77	338.23	2475	1259.8	24.718	1.2222	.4532	815	.00044	1.000	342.5	2.179	.683	102.8
2.00	300.00	2424	1237.9	24.718	1.2228	.4521	802	.00044	1.109	342.5	2.179	.745	111.5
4.00	150.00	2133	1110.7	24.718	1.2299	.4321	741	.00039	1.600	342.5	3.102	1.022	153.5
10.00	60.00	1792	966.4	24.718	1.2401	.4192	659	.00034	2.156	342.5	4.219	1.265	190.0
20.00	30.00	1594	873.0	24.718	1.2499	.4034	599	.00030	2.945	342.5	5.841	1.400	210.3
40.00	15.00	1397	791.7	24.718	1.2611	.3877	540	.00027	2.911	342.5	10.411	1.513	228.9
40.83	14.70	1395	789.5	24.718	1.2614	.3874	539	.00026	2.924	342.5	10.487	1.516	229.9
100.00	6.00	1121	700.6	24.718	1.2747	.3729	467	.00022	3.444	342.5	18.966	1.634	244.4
200.00	3.00	963	642.8	24.718	1.2899	.3581	411	.00019	3.838	342.5	31.744	1.702	253.5
400.00	1.50	813	599.5	24.718	1.3079	.3492	366	.00016	4.283	342.5	52.740	1.743	261.9
1000.00	.60	664	538.4	24.718	1.3199	.3344	303	.00013	4.900	342.5	104.909	1.803	270.8
2000.00	.30	566	506.3	24.718	1.3399	.3266	261	.00011	5.413	342.5	175.109	1.839	276.3
4000.00	.15	471	475.7	24.718	1.3599	.3197	224	.00009	5.973	342.5	286.498	1.868	280.7

TABLE II. - Concluded. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED PRESSURE RATIOS FROM 1 TO 4000 FOR

LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(h) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute; frozen composition during isentropic expansion

Pressure ratio, P _c /P _a	Static pressure, P, lb/in ² abs	Temperature, T, °K	Enthalpy, h, cal/g	Molecular weight, M	Isentropic exponent, γ	Specific heat, C _p , cal/(g)(°K)	Viscosity, μ, micro poises	Thermal conductivity, k, cal/(sec)(°K)(cm)	Mach number, M	Specific impulse in vacuum, I _{vac} , (lb)(sec)/lb	Area ratio, E	Thrust coefficient, C _f	Specific impulse, I, (lb)(sec)/lb
R = 4.000, PERCENT FUEL = 3.054, O/F = 31.746													
1.00	600.00	2381	1054.4	26.323	1.2307	0.4027	806	0.00040	0.000	308.7	2.187	0.000	0.0
1.05	571.43	2359	1045.7	26.323	1.2312	0.4021	801	0.00040	0.282	308.7	2.187	0.204	27.6
1.20	500.00	2300	1022.2	26.323	1.2325	0.4003	788	0.00039	0.549	195.7	1.269	0.392	52.9
1.40	428.57	2234	995.8	26.323	1.2340	0.3981	774	0.00038	0.750	174.2	1.066	0.529	71.4
1.60	375.00	2178	973.6	26.323	1.2353	0.3963	761	0.00037	0.892	169.2	1.011	0.621	83.9
1.79	334.41	2131	954.9	26.323	1.2365	0.3947	750	0.00037	1.000	168.3	1.000	0.689	93.0
2.00	300.00	2087	937.6	26.323	1.2376	0.3932	740	0.00036	1.094	168.8	1.008	0.747	100.8
4.00	150.00	1824	835.4	26.323	1.2452	0.3833	676	0.00032	1.598	181.4	1.286	1.023	138.0
10.00	60.00	1518	720.1	26.323	1.2566	0.3697	595	0.00028	2.155	199.8	2.166	1.263	170.6
20.00	30.00	1315	648.1	26.323	1.2665	0.3588	537	0.00024	2.549	211.4	3.394	1.396	188.5
40.00	15.00	1134	582.1	26.323	1.2771	0.3479	481	0.00021	2.939	221.1	5.444	1.502	202.7
40.83	14.70	1129	580.3	26.323	1.2775	0.3476	480	0.00021	2.951	221.4	5.521	1.505	203.1
100.00	6.00	926	511.0	26.323	1.2927	0.3334	412	0.00018	3.469	231.4	10.356	1.611	217.4
200.00	3.00	789	466.2	26.323	1.3055	0.3226	363	0.00015	3.889	237.7	16.972	1.676	226.2
400.00	1.50	669	428.2	26.323	1.3187	0.3124	317	0.00013	4.336	242.8	27.895	1.729	233.4
1000.00	.60	534	386.7	26.323	1.3363	0.3000	262	0.00010	4.980	248.3	53.871	1.785	241.0
2000.00	.30	447	361.1	26.323	1.3489	0.2918	225	0.00009	5.518	251.6	88.590	1.819	245.6
4000.00	.15	373	339.7	26.323	1.3586	0.2860	191	0.00007	6.112	254.3	145.580	1.847	249.4
R = 5.000, PERCENT FUEL = 2.458, O/F = 39.683													
1.00	600.00	2672	855.0	27.317	1.2436	0.3714	742	0.00034	0.000	282.6	2.194	0.000	0.0
1.05	571.43	2652	847.7	27.317	1.2441	0.3708	737	0.00034	0.281	282.6	2.194	0.205	25.2
1.20	500.00	1999	828.0	27.317	1.2455	0.3691	725	0.00033	0.546	179.0	1.272	0.394	48.5
1.40	428.57	1939	805.9	27.317	1.2472	0.3671	710	0.00033	0.747	159.2	1.068	0.531	65.3
1.60	375.00	1888	787.3	27.317	1.2487	0.3653	698	0.00032	0.888	154.6	1.012	0.623	76.7
1.80	332.87	1844	771.2	27.317	1.2500	0.3637	687	0.00031	1.000	153.7	1.000	0.694	85.4
2.00	300.00	1806	757.4	27.317	1.2512	0.3623	677	0.00031	1.090	154.2	1.007	0.748	92.2
4.00	150.00	1568	672.4	27.317	1.2595	0.3531	614	0.00027	1.594	165.4	1.279	1.023	126.0
10.00	60.00	1294	577.3	27.317	1.2720	0.3402	536	0.00023	2.154	181.8	2.139	1.262	155.4
20.00	30.00	1113	516.7	27.317	1.2824	0.3303	481	0.00020	2.553	192.1	3.335	1.393	171.6
40.00	15.00	953	464.7	27.317	1.2937	0.3204	429	0.00018	2.950	200.7	5.318	1.497	184.3
40.83	14.70	949	463.3	27.317	1.2940	0.3201	428	0.00018	2.962	200.9	5.393	1.499	184.6
100.00	6.00	771	407.4	27.317	1.3104	0.3071	364	0.00014	3.490	209.7	10.039	1.603	197.4
200.00	3.00	652	371.6	27.317	1.3237	0.2975	319	0.00012	3.923	215.2	16.351	1.665	209.1
400.00	1.50	549	341.3	27.317	1.3373	0.2884	277	0.00011	4.385	219.6	26.706	1.717	211.4
1000.00	.60	434	308.7	27.317	1.3544	0.2780	228	0.00008	5.055	224.3	51.154	1.770	218.0
2000.00	.30	361	288.7	27.317	1.3638	0.2727	193	0.00007	5.621	227.1	83.660	1.803	222.0
4000.00	.15	300	272.1	27.317	1.3701	0.2693	163	0.00006	6.245	229.4	136.905	1.829	225.2

TABLE III. - THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS
FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_T	Area ratio, E	Area-ratio exponent, n_E	Specific impulse, I_{sp} , (lb)(sec)/lb	Specific-impulse exponent, n_I	Specific heat, $C_{p, cal/(g)(°K)}$	$(\frac{\partial \ln \eta}{\partial \ln P})_T$	$(\frac{\partial \ln \eta}{\partial \ln T})_P$
R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190									
1.00	1183	0.0000					1.7753	0.00000	0.00000
1.05	1168	.0000	2.250	0.0000	47.4	0.0000	1.7711	.00000	.00000
1.20	1129	.0000	1.297	.0000	90.8	.0000	1.7597	.00000	.00000
1.40	1085	.0000	1.081	.0000	122.2	.0000	1.7472	.00000	.00000
1.60	1049	.0000	1.018	.0000	143.2	.0000	1.7369	.00000	.00000
1.87	1008	.0000	1.000	.0000	163.4	.0000	1.7257	.00000	.00000
2.00	989	.0000	1.003	.0000	171.5	.0000	1.7210	.00000	.00000
4.00	824	.0000	1.233	.0000	232.3	.0000	1.6826	.00000	.00000
4.08	819	.0000	1.244	.0000	233.7	.0000	1.6816	.00000	.00000
10.00	643	.0000	1.974	.0000	283.1	.0000	1.6507	.00000	.00000
20.00	532	.0000	2.983	.0000	309.9	.0000	1.6343	.00000	.00000
40.00	439	.0000	4.620	.0000	330.4	.0000	1.6268	.00000	.00000
100.00	340	.0000	8.432	.0000	350.8	.0000	1.6099	.00000	.00000
200.00	280	.0000	13.431	.0000	362.6	.0000	1.5951	.00000	.00000
400.00	230	.0000	21.488	.0000	372.0	.0000	1.5573	.00000	.00000
1000.00	175	.0000	39.928	.0000	381.6	.0000	1.4871	.00000	.00000
2000.00	142	.0000	63.572	.0000	387.2	.0000	1.4402	.00000	.00000
4000.00	114	.0000	100.939	.0000	391.6	.0000	1.4116	.00000	.00000
R = 3.20, PERCENT FUEL = 38.65, O/F = 1.587									
1.00	1514	0.0000					1.6194	0.00000	-0.0001
1.05	1497	.0000	2.233	0.0000	49.3	0.0000	1.6149	.00000	.0001
1.20	1450	.0000	1.289	.0000	94.6	.0000	1.6028	.00000	.0000
1.40	1398	.0000	1.077	.0000	127.4	.0000	1.5891	.00000	.0000
1.60	1354	.0000	1.016	.0000	149.4	.0000	1.5774	.00000	.0000
1.85	1307	.0000	1.000	.0000	165.2	.0000	1.5653	.00000	.0000
2.00	1282	.0000	1.004	.0000	179.1	.0000	1.5585	.00000	.0000
4.00	1079	.0000	1.244	.0000	243.2	.0000	1.5046	.00000	.0000
4.08	1073	.0000	1.256	.0000	244.7	.0000	1.5031	.00000	.0000
10.00	852	.0000	2.009	.0000	297.2	.0000	1.4516	.00000	.0000
20.00	709	.0000	3.049	.0000	325.9	.0000	1.4232	.00000	.0000
40.00	588	.0000	4.739	.0000	348.0	.0000	1.4067	.00000	.0000
100.00	458	.0000	8.679	.0000	370.0	.0000	1.3916	.00000	.0000
200.00	379	.0000	13.870	.0000	382.7	.0000	1.3807	.00000	.0000
400.00	312	.0000	22.296	.0000	393.0	.0000	1.3681	.00000	.0000
1000.00	242	.0000	41.979	.0000	403.5	.0000	1.3398	.00000	.0000
2000.00	198	.0000	67.687	.0000	409.7	.0000	1.2994	.00000	.0000
4000.00	161	.0000	108.755	.0000	414.6	.0000	1.2564	.00000	.0000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984									
1.00	1816	0.0003					1.5088	0.00004	-0.0013
1.05	1797	.0003	2.218	0.0001	50.3	0.0001	1.5036	.00004	.0002
1.20	1744	.0002	1.283	.0001	96.6	.0001	1.4898	.00003	.0008
1.40	1686	.0001	1.073	.0000	130.1	.0001	1.4751	.00002	.0005
1.60	1636	.0001	1.015	.0000	152.6	.0001	1.4630	.00001	.0004
1.83	1587	.0000	1.000	.0000	171.8	.0001	1.4513	.00001	.0002
2.00	1555	.0000	1.005	.0000	183.1	.0001	1.4436	.00001	.0002
4.00	1322	.0000	1.256	.0000	249.3	.0000	1.3875	.00000	.0000
4.08	1316	.0000	1.268	.0000	250.8	.0000	1.3860	.00000	.0000
10.00	1057	.0000	2.048	.0000	305.6	.0000	1.3426	.00000	.0000
20.00	887	.0000	3.127	.0000	335.7	.0000	1.2848	.00000	.0000
40.00	741	.0000	4.883	.0000	359.0	.0000	1.2559	.00000	.0000
100.00	581	.0000	8.985	.0000	382.4	.0000	1.2321	.00000	.0000
200.00	482	.0000	14.396	.0000	395.9	.0000	1.2190	.00000	.0000
400.00	399	.0000	23.208	.0000	406.8	.0000	1.2100	.00000	.0000
1000.00	310	.0000	43.894	.0000	418.1	.0000	1.1943	.00000	.0000
2000.00	256	.0000	71.279	.0000	424.7	.0000	1.1803	.00000	.0000
4000.00	210	.0000	115.650	.0000	430.2	.0000	1.1487	.00000	.0000
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381									
1.00	2089	0.0017					1.4578	0.00032	-0.0084
1.05	2069	.0015	2.204	0.0007	50.7	0.0007	1.4493	.00028	.0076
1.20	2013	.0011	1.277	.0004	97.4	.0006	1.4276	.00021	.0057
1.40	1950	.0008	1.070	.0002	131.3	.0002	1.4052	.00015	.0041
1.60	1896	.0005	1.013	.0001	154.1	.0004	1.3879	.00010	.0030
1.82	1846	.0004	1.000	.0000	172.5	.0004	1.3729	.00007	.0022
2.00	1808	.0003	1.006	.0001	185.1	.0003	1.3623	.00006	.0017
4.00	1553	.0001	1.266	.0002	252.5	.0002	1.3008	.00001	.0002
4.08	1546	.0001	1.278	.0002	254.1	.0002	1.2992	.00001	.0002
10.00	1258	.0001	2.085	.0002	310.4	.0001	1.2337	.00000	.0000
20.00	1064	.0002	3.207	.0001	341.6	.0001	1.1891	.00000	.0000
40.00	896	.0002	5.038	.0001	365.9	.0001	1.1531	.00000	.0000
100.00	708	.0002	9.326	.0001	390.5	.0000	1.1174	.00000	.0000
200.00	590	.0002	14.995	.0001	404.8	.0000	1.1006	.00000	.0000
400.00	490	.0002	24.237	.0001	416.5	.0000	1.0867	.00000	.0000
1000.00	383	.0002	46.005	.0001	428.3	.0000	1.0745	.00000	.0000
2000.00	317	.0002	74.922	.0001	435.4	.0000	1.0643	.00000	.0000
4000.00	262	.0002	122.202	.0001	441.2	.0000	1.0526	.00000	.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area-ratio exponent, n _ε	Specific impulse, I _c (lb-sec)/lb	Specific impulse exponent, n _I	Specific heat, C _p (cal/g)(°K)	(∂ ln I _c / ∂ ln P) _T	(∂ ln I _c / ∂ ln T) _P
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778									
1.00	2329	0.0052					1.4897	0.00122	-0.0294
1.05	2309	0.0048	2.189	0.0018	50.7	0.0020	1.4752	0.00112	-0.0273
1.20	2253	0.0039	1.270	0.012	97.5	0.018	1.4382	0.00089	-0.0220
1.40	2189	0.0030	1.067	0.007	131.5	0.018	1.3995	0.00067	-0.0170
1.60	2133	0.0023	1.012	0.003	154.4	0.014	1.3707	0.00051	-0.0134
1.80	2085	0.0018	1.000	0.000	171.8	0.012	1.3475	0.00040	-0.0107
2.00	2042	0.0014	1.007	-0.002	185.6	0.012	1.3289	0.00032	-0.0087
4.00	1772	-0.0001	1.277	-0.010	253.8	0.007	1.2391	0.00006	-0.0018
4.08	1764	-0.0001	1.289	-0.010	255.4	0.007	1.2371	0.00005	-0.0017
10.00	1452	-0.0005	2.121	-0.010	312.8	0.004	1.1665	0.00000	-0.0001
20.00	1239	-0.0006	3.285	-0.009	345.0	0.002	1.1208	0.00000	0.0000
40.00	1051	-0.0006	5.194	-0.009	370.1	0.001	1.0795	0.00000	0.0000
100.00	838	-0.0006	9.687	-0.008	395.7	0.001	1.0366	0.00000	0.0000
200.00	703	-0.0006	15.643	-0.008	410.7	0.001	1.0120	0.00000	0.0000
400.00	587	-0.0006	25.377	-0.008	422.9	0.001	0.9954	0.00000	0.0000
1000.00	460	-0.0007	48.339	-0.008	435.5	0.001	0.9790	0.00000	0.0000
2000.00	382	-0.0007	78.934	-0.008	443.0	0.001	0.9694	0.00000	0.0000
4000.00	317	-0.0007	129.082	-0.008	449.2	0.000	0.9600	0.00000	0.0000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175									
1.00	2531	0.0105					1.6075	0.00316	-0.0710
1.05	2512	0.0100	2.173	0.0029	50.4	0.0035	1.5870	0.00296	-0.0671
1.20	2458	0.0086	1.263	0.021	96.9	0.031	1.5334	0.00248	-0.0571
1.40	2396	0.0071	1.053	0.012	130.8	0.034	1.4758	0.00198	-0.0465
1.60	2342	0.0059	1.010	0.005	153.8	0.03	1.4300	0.00162	-0.0390
1.78	2298	0.0050	1.000	0.000	169.9	0.031	1.3954	0.00136	-0.0332
2.00	2252	0.0041	1.008	-0.005	184.9	0.028	1.3620	0.00112	-0.0279
4.00	1978	0.0004	1.289	-0.026	253.7	0.018	1.2147	0.00028	-0.0079
4.08	1970	0.0004	1.302	-0.026	255.3	0.018	1.2116	0.00027	-0.0076
10.00	1640	-0.0011	2.160	-0.031	313.6	0.01	1.1161	0.00003	-0.0009
20.00	1411	-0.0014	3.365	-0.030	346.5	0.006	1.0681	0.00000	-0.0001
40.00	1207	-0.0015	5.356	-0.029	372.4	0.006	1.0259	0.00000	0.0000
100.00	972	-0.0015	10.068	-0.028	398.9	0.004	0.9772	0.00000	0.0000
200.00	820	-0.0016	16.345	-0.028	414.5	0.003	0.9481	0.00000	0.0000
400.00	689	-0.0016	26.628	-0.027	427.3	0.003	0.9252	0.00000	0.0000
1000.00	543	-0.0017	50.955	-0.027	440.6	0.001	0.9041	0.00000	0.0000
2000.00	453	-0.0017	83.421	-0.027	448.5	0.001	0.8930	0.00000	0.0000
4000.00	377	-0.0017	136.777	-0.027	455.1	0.001	0.8834	0.00000	0.0000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571									
1.00	2696	0.0164					1.7899	0.00627	-0.1342
1.05	2678	0.0158	2.159	0.0033	49.9	0.0064	1.7649	0.00597	-0.1286
1.20	2628	0.0143	1.257	0.025	96.0	0.051	1.6982	0.00519	-0.1137
1.40	2570	0.0126	1.060	0.015	129.6	0.05	1.6247	0.00438	-0.0977
1.60	2519	0.0111	1.009	0.006	152.4	0.05	1.5642	0.00374	-0.0849
1.77	2481	0.0100	1.000	0.000	167.2	0.05	1.5208	0.00330	-0.0759
2.00	2434	0.0087	1.010	-0.008	183.5	0.04	1.4702	0.00281	-0.0657
4.00	2167	0.0024	1.303	-0.044	252.4	0.03	1.2440	0.00095	-0.0246
4.08	2159	0.0023	1.316	-0.045	254.0	0.03	1.2389	0.00091	-0.0237
10.00	1822	-0.0016	2.204	-0.064	313.0	0.02	1.0871	0.00013	-0.0040
20.00	1581	-0.0025	3.434	-0.066	346.5	0.01	1.0282	0.00002	-0.0006
40.00	1362	-0.0027	5.529	-0.064	373.1	0.01	0.9843	0.00000	-0.0001
100.00	1109	-0.0029	10.479	-0.062	400.5	0.009	0.9335	0.00000	0.0000
200.00	942	-0.0030	17.107	-0.061	416.8	0.008	0.9005	0.00000	0.0000
400.00	796	-0.0031	28.011	-0.061	430.1	0.008	0.8733	0.00000	0.0000
1000.00	632	-0.0032	53.887	-0.061	444.1	0.006	0.8469	0.00000	0.0000
2000.00	529	-0.0033	88.516	-0.061	452.5	0.006	0.8317	0.00000	0.0000
4000.00	441	-0.0033	145.512	-0.060	459.4	0.006	0.8212	0.00000	0.0000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968									
1.00	2828	0.0218					2.0170	0.01049	-0.2173
1.05	2811	0.0213	2.147	0.0033	49.2	0.007	1.9891	0.01009	-0.2101
1.20	2765	0.0198	1.251	0.024	94.7	0.07	1.9138	0.00904	-0.1908
1.40	2711	0.0181	1.057	0.015	128.0	0.07	1.8287	0.00789	-0.1696
1.60	2664	0.0166	1.008	0.006	150.6	0.07	1.7571	0.00697	-0.1520
1.76	2632	0.0156	1.000	0.000	164.2	0.06	1.7087	0.00637	-0.1403
2.00	2585	0.0140	1.012	-0.009	181.4	0.06	1.6426	0.00557	-0.1247
4.00	2335	0.0062	1.317	-0.055	250.2	0.05	1.3401	0.00237	-0.0580
4.08	2327	0.0060	1.331	-0.056	251.8	0.05	1.3326	0.00230	-0.0565
10.00	1996	-0.0012	2.252	-0.097	311.3	0.03	1.0939	0.00048	-0.0135
20.00	1748	-0.0035	3.552	-0.107	345.4	0.02	1.0036	0.00009	-0.0030
40.00	1518	-0.0043	5.719	-0.107	372.6	0.02	0.9523	0.00001	-0.0004
100.00	1247	-0.0046	10.920	-0.105	400.8	0.01	0.9003	0.00000	0.0000
200.00	1067	-0.0048	17.932	-0.104	417.7	0.01	0.8650	0.00000	0.0000
400.00	907	-0.0050	29.520	-0.103	431.6	0.009	0.8347	0.00000	0.0000
1000.00	727	-0.0052	57.146	-0.103	446.3	0.007	0.8023	0.00000	0.0000
2000.00	611	-0.0053	94.228	-0.103	455.1	0.006	0.7848	0.00000	0.0000
4000.00	512	-0.0054	155.405	-0.103	462.4	0.006	0.7703	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T , °K	Temperature exponent, n_T	Area ratio, ξ	Area ratio exponent, n_ξ	Specific impulse, I , (lb-sec)/lb	Specific impulse exponent, n_I	Specific heat, C_p , cal/(g)°K	$(\frac{\partial \ln M}{\partial \ln P})_T$	$(\frac{\partial \ln M}{\partial \ln T})_P$
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762									
1.00	3015	0.0304					2.5641	0.02196	-0.4374
1.05	3001	0.0300	2.131	0.0026	47.7	0.0108	2.5343	0.02139	-0.4278
1.20	2961	0.0288	1.244	0.0020	51.9	0.0106	2.4522	0.01985	-0.4019
1.40	2914	0.0274	1.054	0.0012	124.2	0.0103	2.3566	0.01813	-0.3722
1.60	2874	0.0262	1.008	0.0005	146.2	0.0101	2.2736	0.01668	-0.3469
1.74	2849	0.0254	1.000	0.0000	158.0	0.0100	2.2225	0.01582	-0.3315
2.00	2807	0.0240	1.014	-0.0008	176.3	0.0097	2.1550	0.01439	-0.3055
4.00	2595	0.0165	1.339	-0.0022	244.1	0.0089	1.7214	0.00892	-0.1889
4.08	2588	0.0162	1.354	-0.0034	245.7	0.0084	1.7099	0.00816	-0.1856
10.00	2299	0.0053	2.346	-0.0120	302.5	0.0067	1.2736	0.00301	-0.0756
20.00	2063	-0.0021	3.762	-0.0165	340.5	0.0054	1.0527	0.00101	-0.0278
40.00	1825	-0.0064	6.136	-0.0169	368.8	0.0042	0.9310	0.00024	-0.0074
100.00	1529	-0.0084	11.885	-0.0195	398.6	0.0030	0.8551	0.00002	-0.0007
200.00	1326	-0.0089	19.729	-0.0193	416.6	0.0024	0.8176	0.00000	-0.0001
400.00	1144	-0.0093	32.844	-0.0192	431.6	0.0019	0.7842	0.00000	0.0000
1000.00	932	-0.0098	64.475	-0.0193	447.7	0.0015	0.7449	0.00000	0.0000
2000.00	792	-0.0101	107.316	-0.0193	457.5	0.0012	0.7201	0.00000	0.0000
4000.00	670	-0.0104	178.419	-0.0194	465.6	0.0010	0.7001	0.00000	0.0000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556									
1.00	3128	0.0362					3.1609	0.03650	-0.7110
1.05	3114	0.0358	2.122	0.0020	46.1	0.0126	3.1356	0.03584	-0.7011
1.20	3078	0.0349	1.240	0.0015	88.9	0.0123	3.0546	0.03406	-0.6738
1.40	3037	0.0339	1.051	0.0009	120.2	0.0123	2.9793	0.03201	-0.6417
1.60	3001	0.0329	1.005	0.0003	141.5	0.0121	2.9028	0.03026	-0.6135
1.74	2981	0.0324	1.000	0.0000	152.2	0.0120	2.8511	0.02927	-0.5973
2.00	2943	0.0313	1.015	-0.0006	170.8	0.0118	2.7698	0.02738	-0.5657
4.00	2761	0.0255	1.353	-0.0040	237.0	0.0108	2.3262	0.01894	-0.4152
4.08	2756	0.0254	1.369	-0.0041	238.6	0.0108	2.3126	0.01870	-0.4108
10.00	2517	0.0160	2.414	-0.0099	297.8	0.0094	1.7290	0.00970	-0.2309
20.00	2320	0.0071	3.943	-0.0155	333.0	0.0082	1.3390	0.00478	-0.1218
40.00	2108	-0.0021	6.551	-0.0215	362.1	0.0069	1.0559	0.00183	-0.0505
100.00	1813	-0.0103	12.932	-0.0265	391.3	0.0053	0.8583	0.00031	-0.0098
200.00	1596	-0.0127	21.699	-0.0276	412.5	0.0042	0.7942	0.00005	-0.0019
400.00	1395	-0.0137	36.494	-0.0277	428.6	0.0034	0.7553	0.00001	-0.0002
1000.00	1156	-0.0146	72.660	-0.0277	446.0	0.0026	0.7136	0.00000	0.0000
2000.00	996	-0.0152	122.229	-0.0279	456.8	0.0022	0.6848	0.00000	0.0000
4000.00	853	-0.0158	205.254	-0.0281	465.9	0.0018	0.6596	0.00000	0.0000
R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349									
1.00	3188	0.0395					3.6135	0.05035	-0.9676
1.05	3175	0.0392	2.117	0.0016	44.6	0.0136	3.5978	0.04974	-0.9597
1.20	3141	0.0385	1.238	0.0012	86.0	0.0133	3.5227	0.04808	-0.9377
1.40	3103	0.0377	1.050	0.0007	116.3	0.0133	3.4573	0.04616	-0.9115
1.60	3070	0.0370	1.005	0.0002	137.0	0.0132	3.4041	0.04449	-0.8880
1.74	3052	0.0366	1.000	0.0000	147.0	0.0131	3.3419	0.04357	-0.8748
2.00	3016	0.0358	1.016	-0.0005	165.3	0.0130	3.2544	0.04169	-0.8472
4.00	2853	0.0317	1.361	-0.0030	229.7	0.0122	3.0181	0.03300	-0.7089
4.08	2848	0.0316	1.376	-0.0030	231.2	0.0122	3.0070	0.03275	-0.7046
10.00	2645	0.0252	2.453	-0.0069	289.2	0.0112	2.4611	0.02178	-0.5040
20.00	2487	0.0188	4.060	-0.0110	324.1	0.0103	1.9810	0.01399	-0.3434
40.00	2321	0.0102	6.873	-0.0166	353.4	0.0093	1.7084	0.00757	-0.1977
100.00	2074	-0.0038	13.944	-0.0261	385.5	0.0078	1.0340	0.00229	-0.0656
200.00	1868	-0.0125	23.785	-0.0319	405.7	0.0063	0.8417	0.00065	-0.0201
400.00	1658	-0.0170	40.475	-0.0345	422.9	0.0054	0.7527	0.00013	-0.0044
1000.00	1398	-0.0191	81.660	-0.0353	441.8	0.0042	0.6975	0.00001	-0.0004
2000.00	1220	-0.0201	138.794	-0.0355	453.6	0.0035	0.6676	0.00000	0.0000
4000.00	1058	-0.0210	235.555	-0.0358	463.7	0.0029	0.6395	0.00000	0.0000
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143									
1.00	3213	0.0410					3.7588	0.05880	-1.1225
1.05	3201	0.0408	2.115	0.0014	43.2	0.0141	3.7501	0.05827	-1.1167
1.20	3168	0.0401	1.238	0.0010	83.2	0.0139	3.7253	0.05683	-1.1004
1.40	3131	0.0394	1.050	0.0005	112.6	0.0138	3.6942	0.05515	-1.0809
1.60	3099	0.0388	1.005	0.0002	137.7	0.0137	3.6652	0.05371	-1.0635
1.74	3082	0.0385	1.000	0.0000	142.2	0.0136	3.6487	0.05293	-1.0538
2.00	3047	0.0378	1.017	-0.0004	160.2	0.0134	3.6123	0.05129	-1.0352
4.00	2892	0.0346	1.364	-0.0024	222.6	0.0128	3.4127	0.04380	-0.9301
4.08	2888	0.0345	1.379	-0.0025	224.1	0.0128	3.4059	0.04358	-0.9269
10.00	2701	0.0300	2.470	-0.0053	280.5	0.0120	3.0540	0.03399	-0.7736
20.00	2564	0.0261	4.112	-0.0077	314.7	0.0115	2.7328	0.02668	-0.6403
40.00	2429	0.0214	7.032	-0.0107	343.6	0.0107	2.3391	0.01951	-0.4947
100.00	2246	0.0125	14.621	-0.0166	375.8	0.0097	1.7259	0.01052	-0.2887
200.00	2095	0.0019	25.591	-0.0241	396.6	0.0088	1.2476	0.00487	-0.1433
400.00	1919	-0.0112	44.582	-0.0335	414.7	0.0077	0.8980	0.00150	-0.0477
1000.00	1660	-0.0216	91.675	-0.0406	435.1	0.0062	0.7114	0.00018	-0.0064
2000.00	1468	-0.0242	157.405	-0.0420	448.0	0.0052	0.6631	0.00003	-0.0010
4000.00	1269	-0.0256	269.819	-0.0424	459.1	0.0045	0.6325	0.00000	-0.0001

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Continued. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P/P _c	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area-ratio exponent, n _ε	Specific impulse, I _s (lb/sec)/lb	Specific-impulse exponent, n _I	Specific heat, C _p cal/(g/°K)	(∂ ln I _s / ∂ ln P) _T	(∂ ln I _s / ∂ ln T) _P
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3217	0.0412							
1.05	3205	+0.410	2.115	0.0014	41.9	0.0141	3.6327	0.06081	-1.1607
1.20	3173	+0.040	1.237	+0.010	80.8	+0.140	3.6262	+0.631	-1.1553
1.40	3136	+0.397	1.050	+0.006	109.3	+0.138	3.5839	+0.5736	-1.1235
1.60	3104	+0.391	1.005	+0.002	128.7	+0.137	3.5618	+0.5599	-1.1080
1.72	3088	+0.388	1.000	+0.000	137.9	+0.136	3.5493	+0.5526	-1.0995
2.00	3053	+0.382	1.017	-0.009	155.4	+0.135	3.5214	+0.5371	-1.0811
4.00	2900	+0.351	1.364	-0.023	216.0	+0.129	3.3683	+0.4671	-0.9903
4.08	2896	+0.350	1.380	-0.024	217.5	+0.129	3.3631	+0.4650	-0.9874
10.00	2713	+0.310	2.474	-0.049	272.3	+0.121	3.1047	+0.3772	-0.8556
20.00	2579	+0.277	4.124	-0.070	305.6	+0.115	2.8627	+0.3120	-0.7448
40.00	2452	+0.242	7.068	-0.092	333.7	+0.109	2.5882	+0.2502	-0.6289
100.00	2287	+0.187	14.785	-0.127	365.2	+0.101	2.1850	+0.1751	-0.4723
200.00	2144	+0.137	26.152	-0.160	385.7	+0.095	1.8612	+0.1248	-0.3562
400.00	2037	+0.075	46.510	-0.202	403.9	+0.089	1.5363	+0.0816	-0.2476
1000.00	1859	-0.030	99.697	-0.277	425.9	+0.079	1.1390	+0.0380	-0.1267
2000.00	1710	-0.127	176.636	-0.348	438.8	+0.070	0.8974	+0.0170	-0.0615
4000.00	1549	-0.219	310.311	-0.417	451.0	+0.061	0.7318	+0.0058	-0.0230
R = 1.50, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3116	0.0362							
1.05	3103	+0.359	2.117	0.0016	37.2	0.0126	2.2973	0.03957	-0.7944
1.20	3070	+0.352	1.238	+0.012	71.6	+0.125	2.2574	+0.3763	-0.7675
1.40	3031	+0.344	1.050	+0.007	96.8	+0.123	2.2216	+0.3601	-0.7443
1.60	2999	+0.336	1.005	+0.002	114.1	+0.122	2.1892	+0.3461	-0.7238
1.72	2981	+0.332	1.000	+0.000	122.4	+0.121	2.1710	+0.3385	-0.7124
2.00	2945	+0.324	1.016	-0.005	137.7	+0.120	2.1323	+0.3230	-0.6887
4.00	2782	+0.284	1.361	-0.029	191.3	+0.112	1.9340	+0.2538	-0.5752
4.08	2777	+0.282	1.377	-0.030	192.6	+0.112	1.9277	+0.2518	-0.5717
10.00	2576	+0.223	2.454	-0.065	240.8	+0.102	1.6300	+0.1698	-0.4190
20.00	2421	+0.168	4.065	-0.099	270.0	+0.094	1.3799	+0.1144	-0.3029
40.00	2263	+0.102	6.896	-0.141	294.4	+0.086	1.1285	+0.0685	-0.1965
100.00	2040	-0.003	14.098	-0.212	321.3	+0.073	0.8344	+0.0264	-0.0862
200.00	1856	-0.082	24.259	-0.267	338.4	+0.063	0.6739	+0.0096	-0.0355
400.00	1664	-0.139	41.606	-0.306	353.1	+0.053	0.5774	+0.0026	-0.0112
1000.00	1415	-0.175	84.484	-0.326	369.3	+0.041	0.5156	+0.0003	-0.0017
2000.00	1240	-0.187	144.082	-0.331	379.5	+0.034	0.4898	+0.0000	-0.0003
4000.00	1080	-0.196	245.360	-0.334	388.2	+0.029	0.4690	+0.0000	0.0000
R = 2.00, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	2966	0.0297							
1.05	2953	+0.294	2.122	0.0019	34.1	0.0107	1.5209	0.02254	-0.4874
1.20	2917	+0.285	1.240	+0.014	65.7	+0.106	1.4788	+0.2210	-0.4802
1.40	2877	+0.275	1.052	+0.008	88.8	+0.104	1.4419	+0.2091	-0.4605
1.60	2841	+0.266	1.005	+0.003	104.6	+0.102	1.4091	+0.1957	-0.4376
1.72	2821	+0.260	1.000	+0.000	112.6	+0.101	1.3901	+0.1842	-0.4178
2.00	2783	+0.250	1.015	-0.006	126.3	+0.099	1.3529	+0.1778	-0.4064
4.00	2604	+0.197	1.353	-0.037	175.2	+0.090	1.1688	+0.1657	-0.3846
4.08	2599	+0.196	1.368	-0.038	176.4	+0.090	1.1632	+0.1630	-0.2831
10.00	2365	+0.117	2.412	-0.087	220.1	+0.078	0.9205	+0.1116	-0.2802
20.00	2177	+0.048	3.941	-0.131	246.1	+0.078	0.7501	+0.0575	-0.1616
40.00	1978	-0.019	6.557	-0.175	267.6	+0.067	0.6166	+0.0286	-0.0890
100.00	1706	-0.080	12.980	-0.214	290.7	+0.056	0.5100	+0.0114	-0.0400
200.00	1505	-0.102	21.822	-0.224	305.0	+0.043	0.4699	+0.0022	-0.0096
400.00	1318	-0.111	36.754	-0.227	316.9	+0.035	0.4457	+0.0005	-0.0024
1000.00	1095	-0.118	73.335	-0.227	329.9	+0.029	0.4457	+0.0001	-0.0005
2000.00	945	-0.123	123.637	-0.228	338.0	+0.022	0.4221	+0.0000	0.0000
4000.00	812	-0.128	208.163	-0.230	344.8	+0.018	0.4064	+0.0000	0.0000
4000.00	812	-0.128	208.163	-0.230	344.8	+0.015	0.3916	+0.0000	0.0000
R = 3.00, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2655	0.0175							
1.05	2640	+0.171	2.140	0.0026	30.2	0.0067	0.8140	0.00697	-0.1761
1.20	2599	+0.160	1.248	+0.019	58.1	+0.065	0.8048	+0.0672	-0.1708
1.40	2550	+0.147	1.056	+0.011	78.5	+0.063	0.7795	+0.0604	-0.1566
1.60	2509	+0.135	1.007	+0.005	92.3	+0.061	0.7506	+0.0531	-0.1408
1.72	2481	+0.127	1.000	+0.000	100.3	+0.059	0.7260	+0.0472	-0.1276
2.00	2438	+0.116	1.013	-0.007	111.3	+0.057	0.7099	+0.0435	-0.1193
4.00	2216	+0.057	1.325	-0.043	153.7	+0.057	0.6858	+0.0382	-0.1070
4.08	2209	+0.055	1.339	-0.044	154.8	+0.046	0.5739	+0.0175	-0.0550
10.00	1915	-0.002	2.286	-0.079	191.7	+0.045	0.5710	+0.0170	-0.0538
20.00	1691	-0.026	3.629	-0.092	213.1	+0.032	0.4712	+0.0044	-0.0165
40.00	1480	-0.036	5.877	-0.095	230.2	+0.024	0.4277	+0.0011	-0.0050
100.00	1229	-0.040	11.319	-0.093	248.1	+0.019	0.4030	+0.0002	-0.0012
200.00	1061	-0.042	18.732	-0.092	258.9	+0.013	0.3820	+0.0000	-0.0001
400.00	911	-0.043	31.103	-0.092	267.9	+0.011	0.3686	+0.0000	0.0000
1000.00	739	-0.045	60.907	-0.092	277.4	+0.009	0.3561	+0.0000	0.0000
2000.00	627	-0.047	101.211	-0.092	283.3	+0.006	0.3403	+0.0000	0.0000
4000.00	529	-0.048	167.951	-0.092	288.1	+0.005	0.3295	+0.0000	0.0000
4000.00	529	-0.048	167.951	-0.092	288.1	+0.004	0.3198	+0.0000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area-ratio exponent, n _ε	Specific impulse, I, (lb)(sec)/lb	Specific-impulse exponent, n _I	Specific heat, c _p , cal/(g)(°K)	(∂ ln Q) _T	(∂ ln Q) _P
R = 4.00, PERCENT FUEL = 3.05, O/F = 1.746									
1.00	2347	0.0079					0.5285	0.00185	-0.0553
1.05	2330	.0075	2.165	0.0021	27.4	0.0032	.5227	.00175	-.0525
1.20	2282	.0066	1.260	.0015	52.7	.0030	.5073	.00147	-.0454
1.40	2228	.0056	1.061	.0009	71.2	.0028	.4906	.00120	-.0380
1.60	2180	.0047	1.009	.0004	83.6	.0026	.4772	.00099	-.0323
1.78	2143	.0041	1.000	.0000	92.1	.0024	.4674	.00085	-.0283
2.00	2101	.0034	1.009	-.0004	100.7	.0023	.4569	.00071	-.0242
4.00	1858	.0006	1.297	-.0021	138.3	.0018	.4102	.00021	-.0084
4.08	1851	.0006	1.311	-.0021	135.2	.0016	.4092	.00020	-.0082
10.70	1556	-.0008	2.192	-.0027	171.3	.0010	.3769	.00003	-.0015
20.30	1351	-.0011	3.439	-.0027	189.6	.0007	.3619	.00000	-.0003
40.00	1167	-.0012	5.518	-.0027	204.1	.0005	.3501	.00000	.0000
100.00	954	-.0013	10.507	-.0026	219.1	.0004	.3354	.00000	.0000
200.00	815	-.0013	17.236	-.0025	228.0	.0003	.3244	.00000	.0000
400.00	692	-.0014	28.358	-.0025	235.4	.0002	.3141	.00000	.0000
1000.00	553	-.0014	54.842	-.0025	243.2	.0002	.3013	.00000	.0000
2000.00	464	-.0015	90.278	-.0025	247.9	.0001	.2929	.00000	.0000
4000.00	387	-.0015	148.471	-.0025	251.7	.0001	.2865	.00000	.0000
R = 5.00, PERCENT FUEL = 2.45, O/F = 9.683									
1.00	2062	0.0027					0.4109	0.00043	-0.0153
1.05	2044	.0025	2.186	0.0010	25.2	0.0011	.4079	.00040	-.0142
1.20	1995	.0020	1.269	.0007	48.4	.0010	.4004	.00032	-.0116
1.40	1938	.0016	1.066	.0004	65.3	.0009	.3925	.00024	-.0091
1.60	1890	.0012	1.011	.0002	76.7	.0008	.3864	.00019	-.0073
1.80	1849	.0010	1.000	.0000	85.1	.0008	.3816	.00015	-.0060
2.00	1811	.0008	1.007	-.0001	92.2	.0007	.3775	.00012	-.0050
4.00	1578	.0000	1.282	-.0005	126.2	.0004	.3579	.00003	-.0013
4.08	1571	.0000	1.295	-.0005	127.0	.0004	.3575	.00002	-.0012
10.00	1304	-.0003	2.145	-.0006	155.7	.0002	.3413	.00000	-.0001
20.00	1122	-.0003	3.345	-.0006	171.9	.0002	.3309	.00000	.0000
40.00	961	-.0003	5.334	-.0005	184.7	.0001	.3209	.00000	.0000
100.00	778	-.0003	10.072	-.0005	197.8	.0001	.3076	.00000	.0000
200.00	659	-.0004	16.410	-.0005	205.6	.0001	.2979	.00000	.0000
400.00	555	-.0004	26.810	-.0005	212.0	.0001	.2888	.00000	.0000
1000.00	438	-.0004	51.370	-.0005	211.6	.0000	.2783	.00000	.0000
2000.00	365	-.0004	84.029	-.0005	222.6	.0000	.2728	.00000	.0000
4000.00	303	-.0004	137.526	-.0005	225.9	.0000	.2693	.00000	.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_2/P_1	Temperature, T, °K	Temperature exponent, η_T	Area ratio, A_2/A_1	Area-ratio exponent, η_A	Specific impulse, I, (lb)sec/lb	Specific-impulse exponent, η_I	Specific heat, C_p , cal/(lb)°K	$(\frac{\partial \ln \eta_T}{\partial \ln P})_T$	$(\frac{\partial \ln \eta_I}{\partial \ln P})_T$
R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190									
1.00	1183	0.0000					1.7752	0.0000	0.0000
1.75	1168	.0000	2.250	0.0000	47.4	0.0000	1.7711	.0000	.0000
1.20	1129	.0000	1.297	.0000	90.8	.0000	1.7597	.0000	.0000
1.40	1085	.0000	1.081	.0000	122.2	.0000	1.7473	.0000	.0000
1.60	1049	.0000	1.018	.0000	143.2	.0000	1.7368	.0000	.0000
1.87	1008	.0000	1.000	.0000	163.4	.0000	1.7257	.0000	.0000
2.00	989	.0000	1.003	.0000	171.5	.0000	1.7210	.0000	.0000
4.00	824	.0000	1.233	.0000	232.3	.0000	1.6825	.0000	.0000
10.00	643	.0000	1.974	.0000	283.1	.0000	1.6505	.0000	.0000
10.21	639	.0000	1.997	.0000	284.0	.0000	1.6501	.0000	.0000
20.00	532	.0000	2.982	.0000	309.9	.0000	1.6343	.0000	.0000
40.00	439	.0000	4.620	.0000	330.4	.0000	1.6269	.0000	.0007
100.00	340	.0000	8.432	.0000	350.8	.0000	1.6091	.0000	.0000
200.00	280	.0000	13.431	.0000	362.6	.0000	1.5971	.0000	.0000
400.00	230	.0000	21.488	.0000	372.0	.0000	1.5856	.0000	.0000
1000.00	175	.0000	39.928	.0000	381.6	.0000	1.4845	.0000	.0000
2000.00	142	.0000	63.572	.0000	387.2	.0000	1.4387	.0000	.0000
4000.00	114	.0000	100.938	.0000	391.6	.0000	1.4054	.0000	.0000
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587									
1.00	1514	0.0000					1.6191	0.0000	-0.0001
1.05	1497	.0000	2.233	0.0000	49.3	0.0000	1.6146	.0000	.0000
1.20	1450	.0000	1.289	.0000	94.6	.0000	1.6026	.0000	.0000
1.40	1398	.0000	1.077	.0000	127.4	.0000	1.5889	.0000	.0000
1.60	1354	.0000	1.016	.0000	149.4	.0000	1.5773	.0000	.0000
1.85	1307	.0000	1.000	.0000	169.2	.0000	1.5652	.0000	.0000
2.00	1282	.0000	1.004	.0000	179.1	.0000	1.5585	.0000	.0000
4.00	1079	.0000	1.244	.0000	243.2	.0000	1.5045	.0000	.0000
10.00	852	.0000	2.009	.0000	297.2	.0000	1.4516	.0000	.0000
10.21	847	.0000	2.033	.0000	298.2	.0000	1.4506	.0000	.0000
20.00	709	.0000	3.049	.0000	325.9	.0000	1.4232	.0000	.0000
40.00	588	.0000	4.739	.0000	348.0	.0000	1.4067	.0000	.0000
100.00	458	.0000	8.679	.0000	370.0	.0000	1.3914	.0000	.0000
200.00	379	.0000	13.870	.0000	382.7	.0000	1.3807	.0000	.0000
400.00	312	.0000	22.295	.0000	393.0	.0000	1.3677	.0000	.0000
1000.00	242	.0000	41.979	.0000	403.5	.0000	1.3402	.0000	.0000
2000.00	198	.0000	67.687	.0000	409.7	.0000	1.2958	.0000	.0000
4000.00	161	.0000	108.754	.0000	414.6	.0000	1.2580	.0000	.0000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984									
1.00	1816	0.0002					1.5040	0.0003	-0.0009
1.05	1797	.0002	2.218	0.0001	50.3	0.0001	1.4992	.00002	-0.0006
1.20	1745	.0001	1.283	.0001	96.6	.0001	1.4867	.00002	-0.0003
1.40	1686	.0001	1.073	.0000	130.1	.0001	1.4730	.00001	-0.0003
1.60	1636	.0000	1.015	.0000	152.7	.0000	1.4616	.00001	-0.0002
1.83	1587	.0000	1.000	.0000	171.8	.0000	1.4503	.00000	-0.0001
2.00	1555	.0000	1.005	.0000	183.1	.0000	1.4429	.00000	-0.0001
4.00	1322	.0000	1.256	.0000	249.3	.0000	1.3875	.00000	.0000
10.00	1057	.0000	2.046	.0000	305.6	.0000	1.3225	.00000	.0000
10.21	1052	.0000	2.073	.0000	306.6	.0000	1.3213	.00000	.0000
20.00	887	.0000	3.127	.0000	335.7	.0000	1.2847	.00000	.0000
40.00	741	.0000	4.883	.0000	359.0	.0000	1.2559	.00000	.0000
100.00	581	.0000	8.985	.0000	382.4	.0000	1.2320	.00000	.0000
200.00	482	.0000	14.396	.0000	395.9	.0000	1.2190	.00000	.0000
400.00	399	.0000	23.208	.0000	406.8	.0000	1.2100	.00000	.0000
1000.00	310	.0000	43.894	.0000	418.1	.0000	1.1953	.00000	.0000
2000.00	256	.0000	71.280	.0000	424.7	.0000	1.1803	.00000	.0000
4000.00	210	.0000	115.651	.0000	430.2	.0000	1.1481	.00000	.0000
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381									
1.00	2092	0.0011					1.4348	0.00020	-0.00054
1.05	2071	.0010	2.205	0.0004	50.8	0.0004	1.4282	.00014	-0.00049
1.20	2015	.0007	1.277	.0003	97.5	.0003	1.4111	.00013	-0.00037
1.40	1951	.0005	1.070	.0002	131.4	.0002	1.3931	.00009	-0.00026
1.60	1897	.0003	1.013	.0001	154.2	.0001	1.3786	.00007	-0.00019
1.82	1846	.0002	1.000	.0000	172.6	.0000	1.3659	.00005	-0.00014
2.00	1809	.0002	1.006	.0000	185.1	.0000	1.3567	.00004	-0.00011
4.00	1553	-.0001	1.266	-.0001	252.5	.0001	1.2999	.00000	-0.0004
10.00	1258	-.0001	2.085	-.0001	310.4	.0001	1.2337	.00000	.0000
10.21	1251	-.0001	2.111	-.0001	311.5	.0001	1.2322	.00000	.0000
20.00	1064	-.0001	3.206	-.0001	341.7	.0001	1.1891	.00000	.0000
40.00	895	-.0001	5.037	-.0001	366.0	.0001	1.1531	.00000	.0000
100.00	708	-.0001	9.325	-.0001	390.5	.0001	1.1175	.00000	.0000
200.00	590	-.0001	14.994	-.0001	404.8	.0001	1.1008	.00000	.0000
400.00	490	-.0001	24.235	-.0001	416.5	.0001	1.0868	.00000	.0000
1000.00	383	-.0001	46.002	-.0001	428.3	.0001	1.0745	.00000	.0000
2000.00	317	-.0001	74.917	-.0001	435.4	.0001	1.0637	.00000	.0000
4000.00	262	-.0001	122.193	-.0001	441.2	.0001	1.0533	.00000	.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_1	Area ratio, E	Area ratio exponent, n_E	Specific impulse, I, (lb-sec)/lb	Specific impulse exponent, n_I	Specific heat, c_p , cal/(lb)(°K)	$(\frac{\partial \ln \eta}{\partial \ln P})_T$	$(\frac{\partial \ln \eta}{\partial \ln T})_P$
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778									
1.00	2339	0.0036					1.4271	0.00081	-0.0194
1.05	2317	0.0033	2.192	0.0012	50.0	0.0014	1.4164	0.00074	-0.0180
1.20	2259	0.0026	1.271	0.0009	97.6	0.0010	1.3889	0.00058	-0.0144
1.40	2195	0.0020	1.067	0.0005	131.6	0.0011	1.3604	0.00043	-0.0110
1.60	2137	0.0015	1.012	0.0004	154.6	0.0010	1.3385	0.00033	-0.0086
1.80	2087	0.0011	1.000	0.0000	172.1	0.0009	1.3209	0.00026	-0.0069
2.00	2044	0.0009	1.007	-0.0001	185.7	0.0008	1.3068	0.00021	-0.0056
4.00	1772	-0.0001	1.276	-0.0006	254.0	0.0003	1.2337	0.00004	-0.0011
10.00	1451	-0.0003	2.120	-0.0005	312.9	0.0003	1.1659	0.00000	-0.0001
10.21	1444	-0.0003	2.147	-0.0006	314.0	0.0003	1.1645	0.00000	-0.0001
20.00	1239	-0.0004	3.282	-0.0006	345.1	0.0002	1.1206	0.00000	0.0000
40.00	1051	-0.0004	5.191	-0.0005	370.2	0.0001	1.0794	0.00000	0.0000
100.00	838	-0.0004	9.681	-0.0005	395.8	0.0001	1.0366	0.00000	0.0000
200.00	702	-0.0004	15.634	-0.0005	410.8	0.0001	1.0119	0.00000	0.0000
400.00	586	-0.0003	25.362	-0.0005	422.9	0.0001	0.9953	0.00000	0.0000
1000.00	460	-0.0004	48.312	-0.0005	435.5	0.0000	0.9789	0.00000	0.0000
2000.00	382	-0.0004	78.890	-0.0005	443.0	0.0000	0.9694	0.00000	0.0000
4000.00	317	-0.0004	129.010	-0.0005	449.2	0.0000	0.9587	0.00000	0.0000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175									
1.00	2553	0.0078					1.4479	0.00219	-0.0489
1.05	2532	0.0074	2.178	0.0022	50.6	0.0029	1.4275	0.00205	-0.0460
1.20	2475	0.0063	1.265	0.0016	97.2	0.0027	1.4323	0.00189	-0.0388
1.40	2410	0.0051	1.064	0.0009	131.2	0.0029	1.3894	0.00134	-0.0315
1.60	2353	0.0041	1.011	0.0004	154.1	0.0023	1.3555	0.00108	-0.0259
1.79	2306	0.0034	1.000	0.0000	170.6	0.0021	1.3293	0.00090	-0.0219
2.00	2260	0.0028	1.008	-0.0004	185.3	0.0020	1.3052	0.00074	-0.0183
4.00	1978	0.0002	1.266	-0.0017	254.0	0.0013	1.1954	0.00018	-0.0050
10.00	1638	-0.0008	2.155	-0.0021	313.9	0.0007	1.1133	0.00002	-0.0005
10.21	1631	-0.0008	2.182	-0.0021	315.0	0.0007	1.1119	0.00001	-0.0005
20.00	1410	-0.0010	3.338	-0.0020	346.7	0.0005	1.0574	0.00000	-0.0001
40.00	1206	-0.0010	5.344	-0.0019	372.5	0.0004	1.0256	0.00000	0.0000
100.00	971	-0.0011	10.047	-0.0018	399.0	0.0003	0.9769	0.00000	0.0000
200.00	819	-0.0011	16.311	-0.0018	414.6	0.0002	0.9479	0.00000	0.0000
400.00	688	-0.0011	26.573	-0.0018	427.4	0.0002	0.9251	0.00000	0.0000
1000.00	543	-0.0011	50.851	-0.0018	440.6	0.0001	0.9040	0.00000	0.0000
2000.00	452	-0.0012	83.253	-0.0018	448.5	0.0001	0.8930	0.00000	0.0000
4000.00	376	-0.0012	136.502	-0.0018	455.1	0.0001	0.8832	0.00000	0.0000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571									
1.00	2733	0.0151					1.6077	0.00457	-0.0965
1.05	2713	0.0126	2.165	0.0030	50.1	0.0044	1.5881	0.00433	-0.0921
1.20	2659	0.0112	1.259	0.0022	98.4	0.0045	1.5361	0.00372	-0.0806
1.40	2596	0.0096	1.061	0.0013	130.2	0.0042	1.4792	0.00309	-0.0684
1.60	2542	0.0083	1.009	0.0006	153.0	0.0040	1.4330	0.00261	-0.0586
1.77	2499	0.0073	1.000	0.0000	168.4	0.0038	1.3991	0.00227	-0.0519
2.00	2451	0.0065	1.009	-0.0006	184.2	0.0036	1.3621	0.00192	-0.047
4.00	2171	0.0014	1.298	-0.0023	253.0	0.0025	1.1951	0.00061	-0.0159
10.00	1819	-0.0015	2.193	-0.0046	315.5	0.0016	1.0768	0.00008	-0.0025
10.21	1812	-0.0015	2.221	-0.0046	314.7	0.0015	1.0750	0.00008	-0.0024
20.00	1578	-0.0018	3.436	-0.0046	346.9	0.0011	1.0258	0.00001	-0.0004
40.00	1359	-0.0020	5.302	-0.0045	373.4	0.0008	0.9635	0.00000	0.0000
100.00	1105	-0.0021	10.428	-0.0043	400.7	0.0006	0.9330	0.00000	0.0000
200.00	939	-0.0022	17.026	-0.0043	417.0	0.0005	0.9001	0.00000	0.0000
400.00	794	-0.0023	27.679	-0.0043	430.2	0.0004	0.8730	0.00000	0.0000
1000.00	631	-0.0023	53.635	-0.0042	444.2	0.0003	0.8467	0.00000	0.0000
2000.00	528	-0.0024	88.103	-0.0042	452.6	0.0002	0.8316	0.00000	0.0000
4000.00	440	-0.0024	144.834	-0.0042	459.5	0.0002	0.8211	0.00000	0.0000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968									
1.00	2881	0.0185					1.7727	0.00757	-0.1623
1.05	2862	0.0179	2.153	0.0032	49.6	0.0066	1.7501	0.00764	-0.1564
1.20	2811	0.0165	1.254	0.0024	95.5	0.0064	1.6893	0.00676	-0.1407
1.40	2752	0.0148	1.059	0.0014	128.6	0.0061	1.6211	0.00583	-0.1234
1.60	2701	0.0133	1.008	0.0006	151.5	0.0058	1.5642	0.00509	-0.1056
1.76	2664	0.0123	1.000	0.0000	165.6	0.0056	1.5246	0.00439	-0.1001
2.00	2615	0.0109	1.011	-0.0008	182.4	0.0054	1.4843	0.00389	-0.0883
4.00	2346	0.0042	1.311	-0.0046	251.2	0.0041	1.2446	0.00159	-0.0386
10.00	1994	-0.0013	2.215	-0.0076	312.2	0.0027	1.0652	0.00030	-0.0084
10.21	1988	-0.0014	2.264	-0.0076	313.3	0.0027	1.0625	0.00029	-0.0080
20.00	1743	-0.0016	3.522	-0.0061	346.1	0.0020	0.9956	0.00006	-0.0018
40.00	1512	-0.0017	5.670	-0.0050	373.2	0.0015	0.9502	0.00001	-0.0003
100.00	1242	-0.0017	10.629	-0.0048	401.3	0.0011	0.8994	0.00000	0.0000
200.00	1063	-0.0016	17.764	-0.0048	418.1	0.0008	0.8642	0.00000	0.0000
400.00	904	-0.0016	27.278	-0.0047	431.9	0.0007	0.840	0.00000	0.0000
1000.00	724	-0.0019	50.676	-0.0047	446.5	0.0005	0.8019	0.00000	0.0000
2000.00	606	-0.0020	83.457	-0.0047	455.3	0.0004	0.7843	0.00000	0.0000
4000.00	510	-0.0021	134.133	-0.0047	462.8	0.0003	0.7700	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I, (lb)(sec)/lb	Specific impulse exponent, n_I	Specific heat, c, cal/(g)(°K)	$(\frac{\partial \ln \eta}{\partial \ln P})_T$	$(\frac{\partial \ln \eta}{\partial \ln T})_P$
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762									
1.00	3097	0.0278	2.136	0.0028	48.2	0.0097	2.2005	0.01775	-0.3453
1.05	3081	0.0273	1.247	0.0021	92.7	0.0095	2.1752	0.01724	-0.3370
1.20	3036	0.0260	1.055	0.0012	125.3	0.0092	2.1055	0.01587	-0.3143
1.40	2985	0.0245	1.007	0.0005	147.5	0.0090	2.0248	0.01435	-0.2887
1.60	2940	0.0232	1.000	0.0000	159.9	0.0088	1.9551	0.01310	-0.2669
1.74	2911	0.0223	1.013	-0.0005	177.6	0.0086	1.9107	0.01232	-0.2533
2.00	2865	0.0208	1.333	-0.0053	245.9	0.0073	1.8396	0.01112	-0.2318
4.00	2630	0.0131	2.321	-0.1113	307.2	0.0056	1.5996	0.00198	-0.0496
10.00	2308	0.0026	2.352	-0.1115	308.4	0.0055	1.1536	0.00192	-0.0483
20.00	2058	-0.0028	3.708	-0.146	342.0	0.0044	1.0010	0.00062	-0.0171
40.00	1815	-0.0056	6.038	-0.159	370.1	0.0034	0.9436	0.00014	-0.0043
100.00	1518	-0.0068	11.693	-0.161	399.6	0.0024	0.8515	0.00001	-0.0004
200.00	1317	-0.0072	19.413	-0.160	417.4	0.0019	0.8157	0.00000	0.0000
400.00	1135	-0.0075	32.319	-0.159	432.3	0.0016	0.7825	0.00000	0.0000
1000.00	924	-0.0079	63.444	-0.159	448.2	0.0012	0.7435	0.00000	0.0000
2000.00	786	-0.0082	105.595	-0.160	457.9	0.0010	0.7189	0.00000	0.0000
4000.00	665	-0.0084	175.548	-0.160	466.0	0.0008	0.6994	0.00000	0.0000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556									
1.00	3231	0.0345	2.126	0.0022	46.7	0.0018	2.7036	0.03093	-0.5863
1.05	3216	0.0342	1.242	0.0016	89.8	0.0017	2.6809	0.03031	-0.5771
1.20	3176	0.0332	1.052	0.0010	121.5	0.0015	2.6171	0.02865	-0.5518
1.40	3130	0.0320	1.008	0.0004	143.1	0.0013	2.5409	0.02672	-0.5222
1.60	3091	0.0309	1.000	0.0000	156.2	0.0012	2.4728	0.02509	-0.4963
1.74	3068	0.0303	1.015	-0.0007	172.6	0.0009	2.4318	0.02414	-0.4809
2.00	3025	0.0291	1.348	-0.0044	239.3	0.0009	2.3550	0.02242	-0.4527
4.00	2823	0.0227	2.391	-0.105	300.2	0.0008	1.9694	0.01481	-0.3188
10.00	2550	0.0123	2.425	-0.107	301.4	0.0008	1.4750	0.00697	-0.1640
10.21	2544	0.0121	3.886	-0.160	335.4	0.0007	1.4650	0.00683	-0.1610
20.00	2331	0.0036	6.425	-0.207	364.2	0.0005	1.1743	0.00316	-0.0601
40.00	2102	-0.0040	12.637	-0.237	395.0	0.0004	0.9713	0.00111	-0.0305
100.00	1797	-0.0095	21.191	-0.241	413.9	0.0003	0.8358	0.00017	-0.0054
200.00	1579	-0.0110	35.638	-0.241	429.6	0.0002	0.7871	0.00003	-0.0010
400.00	1379	-0.0117	64.25	-0.241	429.6	0.0002	0.7520	0.00000	-0.0001
1000.00	1142	-0.0124	119.341	-0.242	447.0	0.0002	0.7111	0.00000	0.0000
2000.00	983	-0.0129	200.371	-0.243	457.6	0.0001	0.6825	0.00000	0.0000
4000.00	841	-0.0134	354.666	-0.245	466.6	0.0001	0.6576	0.00000	0.0000
R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349									
1.00	3304	0.0387	2.121	0.0017	45.2	0.0031	3.1245	0.04443	-0.8285
1.05	3290	0.0384	1.240	0.0012	87.0	0.0029	3.1098	0.04384	-0.8209
1.20	3253	0.0376	1.051	0.0007	117.7	0.0026	3.0677	0.04222	-0.7997
1.40	3211	0.0367	1.005	0.0003	136.6	0.0024	3.0158	0.04055	-0.7744
1.60	3174	0.0359	1.000	0.0000	148.9	0.0023	2.9681	0.03872	-0.7517
1.74	3154	0.0355	1.016	-0.0005	167.3	0.0021	2.9401	0.03781	-0.7387
2.00	3115	0.0345	1.357	-0.0032	232.2	0.0018	2.8824	0.03601	-0.7125
4.00	2935	0.0299	2.437	-0.077	292.0	0.0015	2.5693	0.02763	-0.5803
10.00	2704	0.0224	2.472	-0.078	293.2	0.0014	2.0604	0.01710	-0.3892
10.21	2699	0.0222	4.017	-0.123	327.1	0.0012	2.0482	0.01688	-0.3849
20.00	2526	0.0190	6.763	-0.183	356.3	0.0009	1.6425	0.01020	-0.2476
40.00	2338	0.0066	13.610	-0.265	386.1	0.0008	1.2625	0.00500	-0.1301
100.00	2064	-0.0069	25.116	-0.302	408.0	0.0006	0.9242	0.00131	-0.0377
200.00	1846	-0.0128	39.267	-0.315	424.9	0.0005	0.7993	0.00034	-0.0106
400.00	1634	-0.0155	79.186	-0.318	443.4	0.0004	0.7393	0.00006	-0.0022
1000.00	1375	-0.0169	134.569	-0.320	455.0	0.0003	0.6930	0.00000	-0.0002
2000.00	1199	-0.0177	228.324	-0.322	464.6	0.0002	0.6639	0.00000	0.0000
4000.00	1039	-0.0185	400.371	-0.322	464.6	0.0002	0.6361	0.00000	0.0000
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143									
1.00	3336	0.0406	2.118	0.0015	43.8	0.0036	3.2851	0.05319	-0.9836
1.05	3322	0.0404	1.239	0.0011	84.3	0.0032	3.2773	0.05266	-0.9781
1.20	3286	0.0397	1.051	0.0006	114.0	0.0029	3.2547	0.05127	-0.9629
1.40	3246	0.0389	1.005	0.0003	134.3	0.0026	3.2263	0.04965	-0.9439
1.60	3211	0.0383	1.000	0.0000	144.2	0.0024	3.1957	0.04824	-0.9273
1.74	3192	0.0379	1.016	-0.0004	164.2	0.0022	3.1743	0.04747	-0.9179
2.00	3154	0.0371	1.360	-0.0025	227.2	0.0019	3.1213	0.04589	-0.8993
4.00	2984	0.0323	2.497	-0.080	284.7	0.0016	2.9666	0.03862	-0.7996
10.00	2775	0.0266	2.495	-0.087	284.0	0.0015	2.6006	0.02912	-0.6491
10.21	2770	0.0264	4.054	-0.089	317.9	0.0013	2.5822	0.02891	-0.6459
20.00	2623	0.0241	6.960	-0.118	346.9	0.0010	2.3275	0.02207	-0.5209
40.00	2474	0.0185	14.360	-0.146	375.0	0.0008	1.9960	0.01203	-0.3817
100.00	2267	0.0106	24.792	-0.170	395.0	0.0007	1.3985	0.00709	-0.1940
200.00	2092	0.0040	42.709	-0.171	395.0	0.0006	1.0225	0.00273	-0.0812
400.00	1896	-0.0144	80.419	-0.170	417.0	0.0005	0.8018	0.00073	-0.0234
1000.00	1626	-0.0200	151.906	-0.161	427.4	0.0004	0.6923	0.00008	-0.0029
2000.00	1437	-0.0241	274.745	-0.157	430.0	0.0003	0.6260	0.00001	-0.0004
4000.00	1261	-0.0282	480.371	-0.150	430.0	0.0002	0.6277	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Continued. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, ε	Area ratio exponent, n _ε	Specific impulse, I, (lb)(sec)/lb	Specific impulse exponent, n _I	Specific heat, c _p , cal/(lb)(°K)	(∂ ln I / ∂ ln P) _T	(∂ ln I / ∂ ln T) _P
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3341	0.0410						0.05537	-1.0233
1.05	3328	.0407	2.118	0.0014	42.5	0.0137	3.1852	.05488	-1.0184
1.20	3292	.0401	1.238	.0010	81.8	.0136	3.1796	.05356	-1.0046
1.40	3252	.0394	1.050	.0006	110.7	.0134	3.1421	.05203	-.9883
1.60	3217	.0387	1.005	.0002	130.3	.0133	3.1225	.05071	-.9736
1.72	3199	.0384	1.000	.0000	139.8	.0132	3.1111	.04999	-.9654
2.00	3161	.0377	1.016	-.0004	157.3	.0131	3.0866	.04851	-.9483
4.00	2994	.0344	1.361	-.0024	218.6	.0125	2.9493	.04178	-.8627
10.00	2789	.0299	2.462	-.0051	275.3	.0117	2.7109	.03318	-.7361
10.21	2785	.0298	2.498	-.0051	276.4	.0117	2.7049	.03300	-.7331
20.00	2644	.0264	4.097	-.0073	308.7	.0111	2.4914	.02701	-.6325
40.00	2505	.0224	7.007	-.0097	337.0	.0105	2.2430	.02121	-.5248
100.00	2325	.0164	14.608	-.0135	368.5	.0096	1.8808	.01429	-.3815
200.00	2188	.0108	25.757	-.0172	389.0	.0090	1.5942	.00978	-.2771
400.00	2048	.0040	45.624	-.0218	407.1	.0082	1.3134	.00606	-.1838
1000.00	1850	-.0070	97.111	-.0295	427.8	.0072	.9862	.00255	-.0857
2000.00	1688	-.0158	170.978	-.0360	441.5	.0064	.8018	.00103	-.0380
4000.00	1517	-.0229	298.702	-.0412	453.4	.0055	.6840	.00032	-.0129
R = 1.50, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3219	0.0350						0.03449	-0.6756
1.05	3206	.0347	2.120	0.0017	37.6	0.0120	1.9899	.03400	-.6690
1.20	3169	.0340	1.240	.0012	72.4	.0119	1.9637	.03266	-.6507
1.40	3127	.0331	1.051	.0007	91.9	.0117	1.9320	.03114	-.6292
1.60	3091	.0323	1.005	.0003	115.3	.0116	1.9032	.02983	-.6103
1.72	3071	.0318	1.000	.0000	123.9	.0115	1.8866	.02910	-.5995
2.00	3031	.0309	1.016	-.0005	139.2	.0113	1.8526	.02767	-.5780
4.00	2853	.0265	1.357	-.0030	192.2	.0106	1.6765	.02125	-.4742
10.00	2626	.0199	2.439	-.0069	243.0	.0095	1.4088	.01364	-.3340
10.21	2621	.0197	2.474	-.0070	244.0	.0095	1.4026	.01348	-.3309
20.00	2455	.0140	4.027	-.0105	272.2	.0087	1.1931	.00880	-.2329
40.00	2281	.0071	6.805	-.0149	296.6	.0078	.9827	.00498	-.1440
100.00	2037	-.0027	13.824	-.0214	323.4	.0065	.7495	.00176	-.0586
200.00	1842	-.0092	23.681	-.0258	340.3	.0055	.6298	.00060	-.0229
400.00	1644	-.0133	40.495	-.0284	354.7	.0046	.5593	.00016	-.0071
1000.00	1393	-.0158	82.105	-.0297	370.6	.0036	.5103	.00002	-.0010
2000.00	1220	-.0167	139.978	-.0300	380.6	.0030	.4849	.00000	-.0002
4000.00	1062	-.0175	238.311	-.0302	389.2	.0025	.4666	.00000	.0000
R = 2.00, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	3045	0.0278						0.01897	-0.4038
1.05	3031	.0275	2.126	0.0020	34.4	0.0100	1.3351	.01858	-.3974
1.20	2992	.0266	1.242	.0015	66.3	.0098	1.2984	.01750	-.3799
1.40	2947	.0255	1.052	.0009	89.7	.0096	1.2665	.01629	-.3596
1.60	2909	.0245	1.006	.0003	105.6	.0094	1.2381	.01526	-.3420
1.72	2886	.0239	1.000	.0000	113.8	.0093	1.2211	.01467	-.3316
2.00	2845	.0229	1.015	-.0006	127.4	.0091	1.1894	.01361	-.3127
4.00	2649	.0174	1.348	-.0038	176.6	.0082	1.0314	.00899	-.2244
10.00	2386	.0092	2.393	-.0087	221.6	.0069	.8231	.00434	-.1226
10.21	2382	.0091	2.427	-.0088	222.4	.0069	.8187	.00425	-.1206
20.00	2184	.0028	3.895	-.0128	247.5	.0059	.6852	.00206	-.0650
40.00	1974	-.0028	6.496	-.0164	268.9	.0049	.5809	.00079	-.0282
100.00	1694	-.0074	12.741	-.0192	291.8	.0037	.4985	.00015	-.0066
200.00	1492	-.0090	21.403	-.0199	305.9	.0030	.4656	.00003	-.0017
400.00	1305	-.0057	36.042	-.0200	317.7	.0024	.4438	.00001	-.0003
1000.00	1084	-.0103	71.914	-.0200	330.6	.0019	.4209	.00000	.0000
2000.00	935	-.0107	121.231	-.0201	336.3	.0015	.4053	.00000	.0000
4000.00	803	-.0111	204.087	-.0202	345.2	.0013	.3906	.00000	.0000
R = 3.00, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2695	0.0153						0.00555	-0.1399
1.05	2679	.0149	2.145	0.0025	30.3	0.0059	0.7383	.00533	-.1355
1.20	2634	.0148	1.251	.0018	58.4	.0057	.7094	.00477	-.1236
1.40	2582	.0125	1.057	.0011	78.9	.0054	.6854	.00416	-.1105
1.60	2537	.0114	1.007	.0004	92.8	.0052	.6650	.00368	-.0997
1.72	2507	.0107	1.000	.0000	101.1	.0051	.6513	.00337	-.0927
2.00	2462	.0096	1.012	-.0006	111.9	.0049	.6319	.00295	-.0830
4.00	2226	.0044	1.320	-.0038	154.3	.0038	.5411	.00131	-.0417
10.00	1914	-.0004	2.271	-.0057	192.3	.0027	.4989	.00032	-.0123
10.21	1907	-.0005	2.301	-.0067	193.0	.0026	.4975	.00031	-.0119
20.00	1687	-.0022	3.601	-.0076	213.5	.0020	.4432	.00008	-.0038
40.00	1475	-.0030	5.831	-.0076	230.6	.0015	.4015	.00002	-.0009
100.00	1224	-.0033	11.232	-.0077	248.4	.0011	.3816	.00000	-.0001
200.00	1057	-.0034	18.986	-.0076	259.1	.0009	.3682	.00000	.0000
400.00	908	-.0036	30.867	-.0075	268.1	.0007	.3559	.00000	.0000
1000.00	736	-.0037	60.444	-.0075	277.6	.0005	.3401	.00000	.0000
2000.00	625	-.0039	100.439	-.0075	283.4	.0004	.3292	.00000	.0000
4000.00	527	-.0040	169.664	-.0076	288.2	.0004	.3196	.00000	.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_T	Area ratio, E	Area ratio exponent, n_E	Specific impulse, I_s (lb)(sec)/lb	Specific impulse exponent, n_I	Specific heat, C_p (cal/°K)	$(\frac{\partial \ln \frac{I_s}{P}}{\partial \ln P})_T$	$(\frac{\partial \ln \frac{I_s}{T}}{\partial \ln T})_P$
R = 4.00, PERCENT FUEL = 3.05, O/F = 1.746									
1.00	2363	0.0064					0.5005	0.00142	-0.0427
1.05	2344	.0061	2.169	0.0018	27.5	0.0026	.4958	.00134	-.0405
1.20	2295	.0053	1.261	.0013	52.8	.0024	.4833	.00112	-.0349
1.40	2238	.0044	1.062	.0007	71.3	.0022	.4699	.00091	-.0292
1.60	2188	.0037	1.010	.0003	83.8	.0021	.4590	.00075	-.0247
1.78	2149	.0032	1.000	.0000	92.4	.0020	.4509	.00064	-.0216
2.00	2107	.0027	1.009	-.0003	100.9	.0018	.4426	.00053	-.0185
4.00	1859	.0005	1.295	-.0016	138.5	.0013	.4044	.00016	-.0065
10.00	1555	-.0007	2.187	-.0021	171.5	.0008	.3757	.00002	-.0011
10.21	1544	-.0007	2.215	-.0021	172.1	.0008	.3752	.00002	-.0011
20.00	1350	-.0009	3.431	-.0021	189.7	.0008	.3616	.00000	-.0002
40.00	1166	-.0010	5.506	-.0021	204.2	.0004	.3500	.00000	.0000
100.00	953	-.0010	10.485	-.0020	219.2	.0003	.3353	.00000	.0000
200.00	814	-.0011	17.201	-.0020	228.1	.0004	.3244	.00000	.0000
400.00	691	-.0011	28.301	-.0019	235.5	.0002	.3140	.00000	.0000
1000.00	552	-.0011	54.731	-.0019	243.2	.0001	.3012	.00000	.0000
2000.00	463	-.0012	90.095	-.0020	247.9	.0001	.2928	.00000	.0000
4000.00	387	-.0012	148.169	-.0020	251.7	.0001	.2864	.00000	.0000
R = 5.00, PERCENT FUEL = 2.45, O/F = 9.683									
1.00	2066	0.0021					0.4020	0.00033	-0.0118
1.05	2048	.0020	2.188	0.0008	25.2	0.0009	.3996	.00030	-.0109
1.20	1998	.0016	1.269	.0005	48.4	.0008	.3934	.00024	-.0089
1.40	1941	.0012	1.066	.0003	65.3	.0007	.3869	.00018	-.0070
1.60	1892	.0010	1.011	.0001	76.7	.0006	.3818	.00014	-.0056
1.80	1850	.0007	1.000	.0000	85.2	.0006	.3777	.00011	-.0046
2.00	1812	.0006	1.007	-.0001	92.2	.0005	.3742	.00009	-.0038
4.00	1578	.0000	1.281	-.0004	126.2	.0003	.3570	.00002	-.0010
10.00	1303	-.0002	2.144	-.0005	155.7	.0002	.3411	.00000	-.0001
10.21	1298	-.0002	2.171	-.0005	156.3	.0002	.3408	.00000	-.0001
20.00	1122	-.0002	3.343	-.0004	171.9	.0001	.3309	.00000	.0000
40.00	961	-.0003	5.332	-.0004	184.7	.0001	.3209	.00000	.0000
100.00	778	-.0003	10.068	-.0004	197.9	.0001	.3076	.00000	.0000
200.00	658	-.0003	16.403	-.0004	205.6	.0001	.2979	.00000	.0000
400.00	554	-.0003	26.799	-.0004	212.0	.0000	.2887	.00000	.0000
1000.00	438	-.0003	51.350	-.0004	218.7	.0000	.2782	.00000	.0000
2000.00	365	-.0003	83.996	-.0004	222.6	.0000	.2728	.00000	.0000
4000.00	303	-.0003	137.472	-.0004	225.9	.0000	.2693	.00000	.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P/P ₀	Temperature, T, K	Temperature exponent, n _T	Area ratio, E	Area-ratio exponent, n _E	Specific impulse, I, lbsec/lb	Specific-impulse exponent, n _I	Specific heat, C _p , cal/g ^o C	(∂ ln η_R / ∂ ln P) _T	(∂ ln η_T / ∂ ln T) _P
R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190									
1.00	1183	0.0000	0.0000	0.0000	47.4	0.0000	1.7752	0.00000	0.0000
1.05	1168	0.0000	2.250	0.0000	47.4	0.0000	1.7710	0.00000	0.0000
1.20	1129	0.0000	1.297	0.0000	90.8	0.0000	1.7597	0.00000	0.0000
1.40	1085	0.0000	1.081	0.0000	122.2	0.0000	1.7472	0.00000	0.0000
1.60	1049	0.0000	1.018	0.0000	143.2	0.0000	1.7369	0.00000	0.0000
1.87	1008	0.0000	1.000	0.0000	163.4	0.0000	1.7257	0.00000	0.0000
2.00	989	0.0000	1.003	0.0000	171.5	0.0000	1.7210	0.00000	0.0000
4.00	824	0.0000	1.233	0.0000	232.3	0.0000	1.6825	0.00000	0.0000
10.00	643	0.0000	1.974	0.0000	283.1	0.0000	1.6505	0.00000	0.0000
20.00	532	0.0000	2.982	0.0000	309.9	0.0000	1.6346	0.00000	0.0000
20.41	529	0.0000	3.020	0.0000	310.6	0.0000	1.6339	0.00000	0.0000
40.00	439	0.0000	4.620	0.0000	330.4	0.0000	1.6267	0.00000	0.0000
100.00	340	0.0000	8.432	0.0000	350.8	0.0000	1.6099	0.00000	0.0000
200.00	280	0.0000	13.431	0.0000	362.6	0.0000	1.5970	0.00000	0.0000
400.00	230	0.0000	21.488	0.0000	372.0	0.0000	1.5571	0.00000	0.0000
1000.00	175	0.0000	39.928	0.0000	381.6	0.0000	1.4840	0.00000	0.0000
2000.00	142	0.0000	63.572	0.0000	387.2	0.0000	1.4387	0.00000	0.0000
4000.00	114	0.0000	100.938	0.0000	391.6	0.0000	1.4046	0.00000	0.0000
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587									
1.00	1514	0.0000	0.0000	0.0000	49.3	0.0000	1.6188	0.00000	0.0000
1.05	1497	0.0000	2.233	0.0000	49.3	0.0000	1.6144	0.00000	0.0000
1.20	1450	0.0000	1.289	0.0000	94.6	0.0000	1.6025	0.00000	0.0000
1.40	1398	0.0000	1.077	0.0000	121.4	0.0000	1.5889	0.00000	0.0000
1.60	1354	0.0000	1.016	0.0000	149.4	0.0000	1.5773	0.00000	0.0000
1.85	1307	0.0000	1.000	0.0000	169.2	0.0000	1.5652	0.00000	0.0000
2.00	1282	0.0000	1.004	0.0000	179.1	0.0000	1.5585	0.00000	0.0000
4.00	1079	0.0000	1.244	0.0000	242.2	0.0000	1.5046	0.00000	0.0000
10.00	852	0.0000	2.009	0.0000	297.2	0.0000	1.4516	0.00000	0.0000
20.00	709	0.0000	3.049	0.0000	325.9	0.0000	1.4232	0.00000	0.0000
20.41	705	0.0000	3.088	0.0000	326.7	0.0000	1.4225	0.00000	0.0000
40.00	588	0.0000	4.739	0.0000	348.0	0.0000	1.4065	0.00000	0.0000
100.00	458	0.0000	8.679	0.0000	370.0	0.0000	1.3913	0.00000	0.0000
200.00	379	0.0000	13.870	0.0000	382.7	0.0000	1.3807	0.00000	0.0000
400.00	312	0.0000	22.296	0.0000	393.0	0.0000	1.3677	0.00000	0.0000
1000.00	242	0.0000	41.979	0.0000	403.5	0.0000	1.3402	0.00000	0.0000
2000.00	198	0.0000	67.687	0.0000	409.7	0.0000	1.2977	0.00000	0.0000
4000.00	161	0.0000	106.755	0.0000	414.6	0.0000	1.2571	0.00000	0.0000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984									
1.00	1817	0.0001	0.0000	0.0001	50.3	0.0001	1.5015	0.00002	-0.0006
1.05	1797	0.0001	2.218	0.0001	50.3	0.0001	1.4971	0.00002	-0.0005
1.20	1745	0.0001	1.283	0.0000	96.6	0.0000	1.4852	0.00001	-0.0004
1.40	1686	0.0000	1.073	0.0000	130.1	0.0000	1.4719	0.00001	-0.0002
1.60	1636	0.0000	1.015	0.0000	152.7	0.0000	1.4609	0.00000	-0.0002
1.85	1587	0.0000	1.000	0.0000	171.8	0.0000	1.4498	0.00000	-0.0001
2.00	1555	0.0000	1.005	0.0000	183.1	0.0000	1.4425	0.00000	-0.0001
4.00	1322	0.0000	1.256	0.0000	249.3	0.0000	1.3875	0.00000	0.0000
10.00	1057	0.0000	2.048	0.0000	305.6	0.0000	1.3226	0.00000	0.0000
20.00	887	0.0000	3.127	0.0000	335.7	0.0000	1.2849	0.00000	0.0000
20.41	882	0.0000	3.168	0.0000	336.5	0.0000	1.2838	0.00000	0.0000
40.00	741	0.0000	4.883	0.0000	359.0	0.0000	1.2560	0.00000	0.0000
100.00	581	0.0000	8.985	0.0000	382.4	0.0000	1.2321	0.00000	0.0000
200.00	482	0.0000	14.396	0.0000	395.9	0.0000	1.2192	0.00000	0.0000
400.00	399	0.0000	23.208	0.0000	406.8	0.0000	1.2099	0.00000	0.0000
1000.00	310	0.0000	43.894	0.0000	411.1	0.0000	1.1949	0.00000	0.0000
2000.00	256	0.0000	71.280	0.0000	424.7	0.0000	1.1801	0.00000	0.0000
4000.00	210	0.0000	115.650	0.0000	430.2	0.0000	1.1475	0.00000	0.0000
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381									
1.00	2093	0.0008	0.0000	0.0003	50.8	0.0003	1.4230	0.00014	-0.0038
1.05	2072	0.0007	2.206	0.0003	50.8	0.0003	1.4176	0.00013	-0.0035
1.20	2016	0.0005	1.277	0.0002	97.5	0.0003	1.4027	0.00010	-0.0026
1.40	1952	0.0004	1.070	0.0001	131.4	0.0004	1.3869	0.00007	-0.0019
1.60	1897	0.0004	1.013	0.0000	154.2	0.0004	1.3740	0.00005	-0.0014
1.85	1846	0.0004	1.000	0.0000	172.7	0.0004	1.3623	0.00003	-0.0010
2.00	1809	0.0001	1.006	0.0000	185.1	0.0004	1.3539	0.00003	-0.0008
4.00	1553	0.0000	1.266	0.0001	252.6	0.0001	1.2994	0.00000	-0.0001
10.00	1257	0.0001	2.085	0.0001	310.4	0.0000	1.2335	0.00000	0.0000
20.00	1064	0.0001	3.206	0.0001	341.7	0.0000	1.1891	0.00000	0.0000
20.41	1059	0.0001	3.248	0.0001	342.5	0.0000	1.1878	0.00000	0.0000
40.00	892	0.0001	5.037	0.0001	366.0	0.0000	1.1531	0.00000	0.0000
100.00	707	0.0001	9.325	0.0001	390.5	0.0000	1.1173	0.00000	0.0000
200.00	599	0.0001	14.993	0.0000	405.8	0.0000	1.1006	0.00000	0.0000
400.00	495	0.0001	24.234	0.0000	416.3	0.0000	1.0865	0.00000	0.0000
1000.00	381	0.0001	46.000	0.0000	428.3	0.0000	1.0745	0.00000	0.0000
2000.00	317	0.0001	74.914	0.0000	435.4	0.0000	1.0637	0.00000	0.0000
4000.00	262	0.0001	122.189	0.0000	441.2	0.0000	1.0523	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T , °K	Temperature exponent, n_T	Area ratio, E	Area ratio exponent, n_E	Specific impulse, I_s , (lb-sec)/lb	Specific impulse exponent, n_I	Specific heat, c_p , cal/(g-°K)	$(\frac{\partial \ln \eta}{\partial \ln P})_T$	$(\frac{\partial \ln \eta}{\partial \ln T})_P$
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778									
1.00	2344	0.0026							
1.05	2322	+0.0024	2.194	0.0009	50.9	0.0010	1.3936	0.00059	-0.0141
1.20	2263	+0.0019	1.272	+0.0005	97.7	+0.0009	1.3650	+0.00034	-0.0130
1.40	2196	+0.0014	1.058	+0.0004	131.7	+0.0008	1.3398	+0.00022	-0.0104
1.60	2139	+0.0011	1.012	+0.0001	154.7	+0.0007	1.3219	+0.00024	-0.0079
1.80	2088	+0.0008	1.000	+0.0000	172.3	+0.0006	1.3072	+0.00018	-0.0049
2.00	2045	+0.0006	1.007	+0.0001	185.8	+0.0005	1.2955	+0.00015	-0.0000
4.00	1771	-0.0001	1.275	-0.0004	254.0	+0.0004	1.2510	+0.00003	-0.0008
10.00	1451	-0.0003	2.119	-0.0004	313.0	+0.0004	1.1657	+0.00000	+0.0000
20.00	1238	-0.0003	3.281	-0.0004	345.1	+0.0001	1.1205	+0.00000	+0.0000
20.41	1232	-0.0003	3.325	-0.0004	345.9	+0.0001	1.1192	+0.00000	+0.0000
40.00	1051	-0.0003	5.189	-0.0004	370.2	+0.0001	1.0794	+0.00000	+0.0000
100.00	838	-0.0003	9.678	-0.0004	395.8	+0.0001	1.0365	+0.00000	+0.0000
200.00	702	-0.0003	15.630	-0.0003	410.8	+0.0001	1.0119	+0.00000	+0.0000
400.00	586	-0.0003	25.355	-0.0003	422.9	+0.0000	0.9954	+0.00000	+0.0000
1000.00	460	-0.0003	48.298	-0.0003	435.5	+0.0000	0.9791	+0.00000	+0.0000
2000.00	382	-0.0003	78.868	-0.0003	443.0	+0.0000	0.9692	+0.00000	+0.0000
4000.00	317	-0.0003	128.975	-0.0003	449.2	+0.0000	0.9598	+0.00000	+0.0000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175									
1.00	2565	0.0061							
1.05	2543	+0.0057	2.181	0.0018	50.7	0.0003	1.4207	0.00163	-0.0363
1.20	2484	+0.0048	1.267	+0.0013	97.4	+0.0001	1.4084	+0.00152	-0.0541
1.40	2417	+0.0038	1.065	+0.0007	131.4	+0.0009	1.3764	+0.00125	-0.0286
1.60	2359	+0.0031	1.011	+0.0003	154.4	+0.0007	1.3423	+0.00098	-0.0230
1.79	2310	+0.0025	1.000	+0.0000	171.1	+0.0006	1.3193	+0.00079	-0.0188
2.00	2263	+0.0020	1.008	-0.0003	185.6	+0.0005	1.2941	+0.00065	-0.0158
4.00	1978	+0.0001	1.285	-0.0013	254.2	+0.0003	1.2752	+0.00053	-0.0132
10.00	1637	-0.0006	2.152	-0.0015	314.0	+0.0002	1.1119	+0.00001	-0.0004
20.00	1409	-0.0007	3.354	-0.0014	346.8	+0.0004	1.0671	+0.00000	+0.0000
20.41	1403	-0.0007	3.399	-0.0014	347.6	+0.0004	1.0658	+0.00000	+0.0000
40.00	1205	-0.0008	5.338	-0.0014	372.6	+0.0003	1.0255	+0.00000	+0.0000
100.00	970	-0.0008	10.036	-0.0013	399.1	+0.0002	0.9768	+0.00000	+0.0000
200.00	819	-0.0008	16.294	-0.0013	414.7	+0.0002	0.9478	+0.00000	+0.0000
400.00	687	-0.0008	26.545	-0.0013	427.4	+0.0001	0.9250	+0.00000	+0.0000
1000.00	542	-0.0009	50.799	-0.0013	440.7	+0.0001	0.9038	+0.00000	+0.0000
2000.00	452	-0.0009	83.167	-0.0013	448.6	+0.0001	0.8929	+0.00000	+0.0000
4000.00	376	-0.0009	136.362	-0.0013	455.1	+0.0001	0.8831	+0.00000	+0.0000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571									
1.00	2755	0.0107							
1.05	2734	+0.0102	2.169	0.0026	50.3	0.0009	1.5003	0.00351	-0.0738
1.20	2677	+0.0090	1.261	+0.0019	96.7	+0.0007	1.4843	+0.00332	-0.0702
1.40	2611	+0.0076	1.062	+0.0011	130.5	+0.0004	1.4419	+0.00283	-0.0610
1.60	2555	+0.0065	1.010	+0.0005	153.4	+0.0002	1.3959	+0.00233	-0.0513
1.78	2510	+0.0056	1.000	+0.0000	169.1	+0.0000	1.3888	+0.00195	-0.0438
2.00	2460	+0.0048	1.009	-0.0005	184.6	+0.0000	1.3312	+0.00168	-0.0384
4.00	2173	+0.0010	1.295	-0.0026	257.4	+0.0000	1.3023	+0.00142	-0.0329
10.00	1818	-0.0010	2.187	-0.0035	313.8	+0.0002	1.1697	+0.00044	-0.0113
20.00	1576	-0.0014	3.427	-0.0034	347.2	+0.0009	1.0717	+0.00006	-0.0017
20.41	1569	-0.0014	3.474	-0.0034	348.1	+0.0009	1.0246	+0.00001	-0.0003
40.00	1358	-0.0015	5.487	-0.0033	373.6	+0.0006	1.0233	+0.00001	-0.0003
100.00	1105	-0.0016	10.401	-0.0032	400.9	+0.0005	0.9831	+0.00000	+0.0000
200.00	938	-0.0017	16.983	-0.0032	417.1	+0.0004	0.9327	+0.00000	+0.0000
400.00	793	-0.0017	27.808	-0.0032	430.3	+0.0003	0.8999	+0.00000	+0.0000
1000.00	630	-0.0018	53.499	-0.0032	444.3	+0.0002	0.8728	+0.00000	+0.0000
2000.00	527	-0.0018	87.879	-0.0032	452.6	+0.0002	0.8465	+0.00000	+0.0000
4000.00	440	-0.0018	144.468	-0.0031	459.5	+0.0001	0.8315	+0.00000	+0.0000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968									
1.00	2915	0.0198							
1.05	2895	+0.0193	2.158	0.0029	49.8	0.0006	1.6231	0.00633	-0.1275
1.20	2841	+0.0139	1.256	+0.0022	95.7	+0.0004	1.6042	+0.00604	-0.1225
1.40	2778	+0.0123	1.060	+0.0013	129.5	+0.0001	1.5535	+0.00531	-0.1093
1.60	2724	+0.0109	1.007	+0.0006	152.0	+0.0009	1.4970	+0.00494	-0.0923
1.77	2684	+0.0099	1.000	+0.0000	166.6	+0.0007	1.4502	+0.00393	-0.0837
2.00	2633	+0.0087	1.010	-0.0007	183.0	+0.0004	1.4168	+0.00351	-0.0760
4.00	2352	+0.0030	1.307	-0.0039	251.9	+0.0003	1.3768	+0.00303	-0.0667
10.00	1992	-0.0017	2.224	-0.0061	312.7	+0.0001	1.1732	+0.00116	-0.0281
20.00	1740	-0.0023	3.304	-0.0064	346.6	+0.0006	1.0508	+0.00021	-0.0059
20.41	1732	-0.0023	3.353	-0.0064	347.5	+0.0006	0.9916	+0.00004	-0.0012
40.00	1509	-0.0026	5.642	-0.0063	373.5	+0.0002	0.9702	+0.00001	-0.0002
100.00	1240	-0.0028	10.777	-0.0061	401.5	+0.0008	0.9491	+0.00000	+0.0000
200.00	1060	-0.0029	17.699	-0.0061	418.5	+0.0007	0.8988	+0.00000	+0.0000
400.00	902	-0.0029	29.139	-0.0060	432.1	+0.0005	0.8638	+0.00000	+0.0000
1000.00	722	-0.0031	56.410	-0.0060	446.6	+0.0003	0.8336	+0.00000	+0.0000
2000.00	607	-0.0032	93.015	-0.0060	455.4	+0.0003	0.8015	+0.00000	+0.0000
4000.00	508	-0.0033	153.404	-0.0060	462.7	+0.0003	0.7842	+0.00000	+0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_s , (lb)(sec)/lb	Specific-impulse exponent, n_I	Specific heat, C_{p1} , cal/(lb)(°K)	$(\frac{\partial \ln \eta}{\partial \ln P})_T$	$(\frac{\partial \ln \eta}{\partial \ln T})_P$
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762									
1.00	3155	0.0254					1.9667	0.01480	-0.2833
1.05	3137	+0.249	2.140	0.0028	48.5	0.0088	1.9446	+0.1434	-0.2759
1.20	3089	+0.235	1.248	+0.021	95.3	+0.085	1.8842	+0.1312	-0.2559
1.40	3033	+0.220	1.056	+0.013	126.1	+0.083	1.8145	+0.1177	-0.2335
1.60	2985	+0.206	1.007	+0.005	148.4	+0.080	1.7545	+0.1067	-0.2145
1.75	2953	+0.197	1.000	+0.000	161.2	+0.079	1.7154	+0.0997	-0.2024
2.00	2904	+0.182	1.013	-0.008	178.8	+0.076	1.6559	+0.0894	-0.1843
4.00	2652	+0.106	1.328	-0.051	247.0	+0.064	1.3741	+0.0466	-0.1037
10.00	2311	+0.015	2.303	-0.104	308.3	+0.047	1.0984	+0.0142	-0.0356
20.00	2054	-0.029	3.673	-0.127	343.0	+0.036	0.9752	+0.0045	-0.0118
20.41	2047	-0.029	3.726	-0.128	343.9	+0.036	0.9726	+0.0041	-0.0113
40.00	1808	-0.049	5.977	-0.136	370.9	+0.028	0.9053	+0.0009	-0.0029
100.00	1512	-0.058	11.573	-0.136	400.2	+0.020	0.8496	+0.0001	-0.0003
200.00	1311	-0.061	19.216	-0.135	418.0	+0.016	0.8145	+0.0000	+0.0007
400.00	1130	-0.063	31.993	-0.134	432.7	+0.013	0.7815	+0.0000	+0.0000
1000.00	919	-0.066	62.803	-0.134	448.6	+0.010	0.7427	+0.0000	+0.0000
2000.00	782	-0.059	104.524	-0.135	458.2	+0.008	0.7183	+0.0000	+0.0000
4000.00	661	-0.071	173.763	-0.135	466.3	+0.007	0.6988	+0.0000	+0.0000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556									
1.00	3307	0.0328					2.3992	0.02681	-0.4983
1.05	3291	+0.324	2.129	0.0023	47.0	0.0111	2.3785	+0.02623	-0.4898
1.20	3248	+0.314	1.244	+0.017	90.6	+0.109	2.3204	+0.2465	-0.4663
1.40	3198	+0.301	1.053	+0.010	122.4	+0.107	2.2512	+0.2286	-0.4389
1.60	3156	+0.289	1.006	+0.004	144.1	+0.105	2.1898	+0.2134	-0.4151
1.75	3130	+0.282	1.000	+0.000	155.6	+0.104	2.1520	+0.2044	-0.4007
2.00	3085	+0.269	1.014	-0.007	173.9	+0.102	2.0841	+0.1889	-0.3752
4.00	2865	+0.201	1.344	-0.046	240.8	+0.091	1.7441	+0.1201	-0.2554
10.00	2569	+0.095	2.374	-0.108	301.9	+0.075	1.3258	+0.0529	-0.1237
20.00	2335	+0.015	3.843	-0.156	336.9	+0.063	1.0849	+0.0226	-0.0572
20.41	2328	+0.013	3.900	-0.156	337.9	+0.062	1.0791	+0.0219	-0.0557
40.00	2095	-0.047	6.337	-0.193	365.6	+0.051	0.9294	+0.0075	-0.0206
100.00	1785	-0.086	12.441	-0.212	396.1	+0.038	0.8253	+0.0011	-0.0033
200.00	1568	-0.097	20.858	-0.214	414.9	+0.030	0.7835	+0.0002	-0.0006
400.00	1368	-0.102	39.080	-0.214	430.6	+0.025	0.7500	+0.0000	-0.0001
1000.00	1133	-0.108	69.841	-0.214	447.6	+0.019	0.7094	+0.0000	+0.0000
2000.00	975	-0.113	117.461	-0.215	458.2	+0.016	0.6811	+0.0000	+0.0000
4000.00	834	-0.117	197.192	-0.217	467.0	+0.013	0.6564	+0.0000	+0.0000
R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349									
1.00	3393	0.0377					2.7921	0.03590	-0.7279
1.05	3378	+0.374	2.123	0.0018	45.6	0.0126	2.7781	+0.03593	-0.7206
1.20	3338	+0.366	1.241	+0.013	87.8	+0.124	2.7382	+0.3775	-0.7001
1.40	3292	+0.356	1.052	+0.008	118.7	+0.122	2.6891	+0.3593	-0.6756
1.60	3253	+0.347	1.005	+0.003	139.8	+0.121	2.6439	+0.3435	-0.6538
1.75	3231	+0.342	1.000	+0.000	150.4	+0.120	2.6168	+0.3345	-0.6410
2.00	3189	+0.332	1.015	-0.005	168.7	+0.118	2.5628	+0.3173	-0.6167
4.00	2995	+0.282	1.354	-0.034	234.0	+0.110	2.2689	+0.2369	-0.4897
10.00	2744	+0.199	2.423	-0.083	294.1	+0.098	1.8019	+0.1386	-0.3122
20.00	2550	+0.118	3.982	-0.132	329.1	+0.088	1.4368	+0.0779	-0.1878
20.41	2544	+0.116	4.042	-0.134	330.1	+0.087	1.4265	+0.0763	-0.1844
40.00	2344	+0.025	6.676	-0.191	358.3	+0.076	1.1265	+0.0355	-0.0922
100.00	2053	-0.080	13.365	-0.258	389.8	+0.060	0.8717	+0.0085	-0.0245
200.00	1830	-0.123	22.652	-0.282	409.5	+0.050	0.7805	+0.0021	-0.0066
400.00	1617	-0.141	38.453	-0.289	426.2	+0.041	0.7331	+0.0004	-0.0013
1000.00	1360	-0.152	77.533	-0.291	444.4	+0.031	0.6903	+0.0000	-0.0001
2000.00	1185	-0.159	131.747	-0.292	455.9	+0.026	0.6615	+0.0000	+0.0000
4000.00	1027	-0.166	223.495	-0.294	465.6	+0.022	0.6339	+0.0000	+0.0000
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143									
1.00	3430	0.0401					2.9626	0.04890	-0.8833
1.05	3416	+0.393	2.121	0.0015	44.2	0.0132	2.9553	+0.04840	-0.8780
1.20	3377	+0.391	1.240	+0.011	85.1	+0.131	2.9343	+0.4704	-0.8631
1.40	3334	+0.383	1.051	+0.006	111.1	+0.129	2.9078	+0.4546	-0.8452
1.60	3296	+0.376	1.005	+0.002	135.5	+0.128	2.8830	+0.4409	-0.8291
1.75	3276	+0.372	1.000	+0.000	145.6	+0.127	2.8682	+0.4332	-0.8199
2.00	3235	+0.364	1.016	-0.004	163.6	+0.126	2.8374	+0.4160	-0.8012
4.00	3054	+0.326	1.358	-0.026	227.1	+0.119	2.6636	+0.3473	-0.7059
10.00	2829	+0.271	2.448	-0.058	285.8	+0.110	2.3536	+0.2551	-0.5605
20.00	2666	+0.222	4.058	-0.088	320.2	+0.103	2.0547	+0.1871	-0.4366
20.41	2661	+0.220	4.121	-0.089	321.2	+0.103	2.0450	+0.1851	-0.4328
40.00	2503	+0.158	6.901	-0.128	349.2	+0.095	1.7023	+0.1221	-0.3040
100.00	2276	+0.037	14.187	-0.208	381.3	+0.083	1.2030	+0.0498	-0.1364
200.00	2084	-0.074	24.518	-0.284	401.7	+0.073	0.9125	+0.0171	-0.0508
400.00	1877	-0.152	42.200	-0.336	419.4	+0.061	0.7617	+0.0042	-0.0136
1000.00	1606	-0.192	86.184	-0.357	439.0	+0.048	0.6840	+0.0004	-0.0016
2000.00	1416	-0.204	147.806	-0.361	451.3	+0.040	0.6520	+0.0001	-0.0002
4000.00	1241	-0.213	253.224	-0.363	462.0	+0.034	0.6246	+0.0000	+0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Continued. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_T	Area ratio, ϵ	Area-ratio exponent, n_ϵ	Specific impulse, I_s (lbsec/lb)	Specific-impulse exponent, n_{I_s}	Specific heat, C_p (cal/(g°K))	$\left(\frac{\partial \ln \bar{M}}{\partial \ln P}\right)_T$	$\left(\frac{\partial \ln \bar{M}}{\partial \ln T}\right)_P$
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3437	0.0405					2.8811	0.05123	-0.9244
1.05	3423	0.0403	2.120	0.0014	42.9	0.0133	2.8760	0.05076	-0.9197
1.20	3384	0.0396	1.239	0.0010	82.6	0.0122	2.8611	0.04948	-0.9057
1.40	3341	0.0389	1.051	0.0006	111.7	0.0111	2.8421	0.04800	-0.8912
1.60	3304	0.0382	1.005	0.0002	131.5	0.0109	2.8263	0.04672	-0.8773
1.72	3284	0.0378	1.000	0.0000	141.3	0.0109	2.8138	0.04601	-0.8693
2.00	3244	0.0371	1.016	-0.0004	158.0	0.0107	2.7914	0.04460	-0.8532
4.00	3065	0.0356	1.359	-0.0024	220.4	0.011	2.6657	0.03811	-0.7719
10.00	2847	0.0289	2.453	-0.0052	277.5	0.013	2.4459	0.02986	-0.6519
20.00	2692	0.0251	4.076	-0.0075	311.1	0.017	2.2431	0.02398	-0.5541
20.41	2687	0.0250	4.140	-0.0075	312.0	0.016	2.2367	0.02381	-0.5512
40.00	2542	0.0209	6.959	-0.0100	339.4	0.010	2.0143	0.01851	-0.4532
100.00	2349	0.0144	14.469	-0.0141	370.9	0.002	1.6831	0.01209	-0.3207
200.00	2203	0.0084	25.445	-0.0180	391.3	0.005	1.4246	0.00801	-0.2266
400.00	2052	0.0014	44.925	-0.0228	409.3	0.007	1.1770	0.00475	-0.1443
1000.00	1839	-0.0094	95.113	-0.0303	429.9	0.007	0.8997	0.00185	-0.0626
2000.00	1668	-0.0171	166.760	-0.0360	443.3	0.008	0.7520	0.00070	-0.0260
4000.00	1493	-0.0227	290.406	-0.0400	455.0	0.005	0.6606	0.00020	-0.0083
R = 1.50, PERCENT FUEL = 7.74, O/F = 1.905									
1.00	3297	0.0338					1.8003	0.03075	-0.5921
1.05	3282	0.0335	2.123	0.0017	37.9	0.013	1.7919	0.03029	-0.5859
1.20	3243	0.0327	1.241	0.0012	75.0	0.014	1.7680	0.02902	-0.5689
1.40	3198	0.0318	1.052	0.0007	98.7	0.012	1.7391	0.02758	-0.5480
1.60	3159	0.0309	1.005	0.0003	116.2	0.010	1.7131	0.02635	-0.5312
1.73	3137	0.0304	1.000	0.0000	125.0	0.010	1.6977	0.02565	-0.5240
2.00	3096	0.0295	1.015	-0.0005	140.2	0.010	1.6672	0.02432	-0.5012
4.00	2904	0.0249	1.354	-0.0031	194.6	0.010	1.5078	0.01834	-0.4053
10.00	2661	0.0179	2.427	-0.0071	244.6	0.009	1.2677	0.01140	-0.2780
20.00	2478	0.0118	3.997	-0.0108	273.8	0.008	1.0774	0.00711	-0.1886
20.41	2472	0.0116	4.058	-0.0110	274.6	0.008	1.0719	0.00700	-0.1862
40.00	2291	0.0050	6.734	-0.0151	298.2	0.001	0.8963	0.00387	-0.1126
100.00	2032	-0.0040	13.621	-0.0211	324.8	0.003	0.7030	0.00129	-0.0437
200.00	1830	-0.0093	23.271	-0.0245	341.5	0.004	0.6070	0.00043	-0.0167
400.00	1629	-0.0125	39.732	-0.0264	355.8	0.001	0.5500	0.00011	-0.0051
1000.00	1379	-0.0144	80.499	-0.0273	371.5	0.002	0.5072	0.00001	-0.0007
2000.00	1207	-0.0152	137.214	-0.0276	381.4	0.007	0.4850	0.00000	-0.0001
4000.00	1050	-0.0159	233.567	-0.0278	389.8	0.002	0.4650	0.00000	0.0000
R = 2.00, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	3103	0.0262					1.2138	0.01648	-0.3472
1.05	3088	0.0258	2.129	0.0020	34.7	0.0003	1.2052	0.01611	-0.3414
1.20	3046	0.0249	1.243	0.0015	66.7	0.002	1.1812	0.01513	-0.3255
1.40	2998	0.0237	1.053	0.0009	90.2	0.000	1.1528	0.01402	-0.3072
1.60	2957	0.0228	1.006	0.0003	106.2	0.008	1.1276	0.01309	-0.2914
1.73	2932	0.0222	1.000	0.0000	114.7	0.007	1.1122	0.01255	-0.2819
2.00	2889	0.0211	1.014	-0.0006	128.2	0.005	1.0844	0.01160	-0.2651
4.00	2679	0.0155	1.344	-0.0038	177.5	0.005	0.9449	0.00749	-0.1868
10.00	2402	0.0075	2.379	-0.0086	222.6	0.003	0.7644	0.00348	-0.0990
20.00	2188	0.0017	3.861	-0.0123	248.5	0.003	0.6477	0.00160	-0.0512
20.41	2181	0.0015	3.918	-0.0124	249.2	0.002	0.6467	0.00156	-0.0501
40.00	1970	-0.0031	6.385	-0.0153	265.8	0.003	0.5611	0.00060	-0.0218
100.00	1686	-0.0068	12.580	-0.0174	292.5	0.003	0.4923	0.00012	-0.0051
200.00	1483	-0.0080	21.125	-0.0179	306.5	0.006	0.4632	0.00003	-0.0013
400.00	1297	-0.0086	35.572	-0.0180	318.2	0.001	0.4427	0.00000	-0.0004
1000.00	1076	-0.0092	70.973	-0.0180	331.0	0.006	0.4201	0.00000	0.0000
2000.00	929	-0.0095	119.641	-0.0180	338.9	0.004	0.4046	0.00000	0.0000
4000.00	797	-0.0099	201.392	-0.0182	345.5	0.001	0.3900	0.00000	0.0000
R = 3.00, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2723	0.0136					0.6909	0.00463	-0.1169
1.05	2705	0.0132	2.148	0.0023	30.5	0.0002	0.6842	0.00445	-0.1131
1.20	2658	0.0122	1.252	0.0017	58.6	0.000	0.6659	0.00396	-0.1029
1.40	2604	0.0110	1.058	0.0010	79.2	0.008	0.6451	0.00344	-0.0917
1.60	2556	0.0100	1.008	0.0004	93.1	0.006	0.6275	0.00303	-0.0825
1.73	2523	0.0093	1.000	0.0000	101.6	0.005	0.6155	0.00276	-0.0763
2.00	2477	0.0083	1.012	-0.0006	112.2	0.003	0.5991	0.00241	-0.0682
4.00	2232	0.0056	1.317	-0.0034	154.7	0.003	0.5216	0.00106	-0.0338
10.00	1914	-0.0005	2.261	-0.0058	192.6	0.003	0.4517	0.00026	-0.0099
20.00	1684	-0.0020	3.584	-0.0065	213.8	0.007	0.4206	0.00007	-0.0030
20.41	1678	-0.0020	3.634	-0.0065	214.4	0.007	0.4199	0.00006	-0.0029
40.00	1472	-0.0026	5.802	-0.0066	230.8	0.003	0.4007	0.00001	-0.0007
100.00	1222	-0.0028	11.177	-0.0065	248.6	0.009	0.3813	0.00000	-0.0001
200.00	1055	-0.0030	18.498	-0.0065	259.3	0.007	0.3680	0.00000	0.0000
400.00	906	-0.0031	30.718	-0.0064	268.2	0.006	0.3557	0.00000	0.0000
1000.00	735	-0.0032	60.134	-0.0064	277.7	0.005	0.3399	0.00000	0.0000
2000.00	623	-0.0033	95.956	-0.0064	283.5	0.004	0.3291	0.00000	0.0000
4000.00	526	-0.0034	165.857	-0.0065	288.3	0.003	0.3195	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, η _T	Area ratio, E	Area-ratio exponent, η _E	Specific impulse, I, (lb)sec/lb	Specific-impulse exponent, η _I	Specific heat, C _p , cal/(g)(°K)	(∂ ln I / ∂ ln P) _T	(∂ ln I / ∂ ln T) _P
R = 4.00, PERCENT FUEL = 3.09, O/F = 1.746									
1.00	2372	0.0055					0.4836	0.00116	-0.0351
1.05	2354	+0.0052	2.172	0.0015	27.5	0.0022	4.796	+0.0109	-0.0359
1.20	2303	+0.0045	1.262	+0.011	52.9	+0.021	4.689	+0.0091	-0.0287
1.40	2244	+0.0037	1.065	+0.006	71.4	+0.019	4.574	+0.0074	-0.0239
1.60	2194	+0.0021	1.010	+0.003	83.9	+0.018	4.481	+0.0061	-0.0203
1.78	2153	+0.0027	1.000	+0.000	92.6	+0.017	4.412	+0.0052	-0.0177
2.00	2110	+0.0022	1.009	+0.003	101.0	+0.016	4.341	+0.0043	-0.0151
4.00	1859	+0.0004	1.294	+0.013	139.6	+0.011	4.010	+0.0013	-0.0053
10.00	1555	+0.0006	2.184	+0.018	171.6	+0.006	3.749	+0.0002	-0.0009
20.00	1349	+0.0007	3.426	+0.018	189.8	+0.005	3.614	+0.0000	-0.0002
20.41	1343	+0.0008	3.474	+0.018	190.2	+0.005	3.611	+0.0000	-0.0002
40.00	1165	+0.0008	5.499	+0.017	204.2	+0.003	3.499	+0.0000	-0.0000
100.00	952	+0.0009	10.472	+0.016	219.2	+0.002	3.352	+0.0000	-0.0000
200.00	813	+0.0009	17.179	+0.016	228.1	+0.002	3.243	+0.0000	-0.0000
400.00	690	+0.0009	28.266	+0.016	235.5	+0.002	3.139	+0.0000	-0.0000
1000.00	552	+0.0009	54.663	+0.016	243.2	+0.001	3.012	+0.0000	-0.0000
2000.00	463	+0.0010	89.984	+0.016	247.9	+0.001	2.928	+0.0000	-0.0000
4000.00	386	+0.0010	147.985	+0.016	251.8	+0.001	2.864	+0.0000	-0.0000
R = 5.00, PERCENT FUEL = 2.45, O/F = 9.683									
1.00	2069	0.0018					0.3968	0.00027	-0.0097
1.05	2051	+0.0016	2.189	0.0006	25.2	0.0007	3.947	+0.0025	-0.0090
1.20	2000	+0.0013	1.270	+0.004	48.5	+0.007	3.893	+0.0020	-0.0074
1.40	1942	+0.0010	1.066	+0.002	65.4	+0.006	3.835	+0.0015	-0.0058
1.60	1893	+0.0008	1.011	+0.001	76.8	+0.005	3.790	+0.0012	-0.0046
1.80	1851	+0.0006	1.000	+0.000	85.3	+0.005	3.753	+0.0009	-0.0038
2.00	1813	+0.0005	1.007	+0.001	92.2	+0.005	3.722	+0.0008	-0.0032
4.00	1578	+0.0000	1.281	+0.003	126.2	+0.003	3.564	+0.0002	-0.0008
10.00	1303	+0.0002	2.143	+0.004	155.8	+0.002	3.411	+0.0000	-0.0001
20.00	1122	+0.0002	3.342	+0.004	172.0	+0.001	3.309	+0.0000	-0.0000
20.41	1117	+0.0002	3.386	+0.004	172.4	+0.001	3.306	+0.0000	-0.0000
40.00	961	+0.0002	5.330	+0.003	184.7	+0.001	3.209	+0.0000	-0.0000
100.00	777	+0.0002	10.066	+0.003	197.9	+0.001	3.076	+0.0000	-0.0000
200.00	658	+0.0002	16.399	+0.003	205.7	+0.000	2.979	+0.0000	-0.0000
400.00	554	+0.0002	26.792	+0.003	212.0	+0.000	2.887	+0.0000	-0.0000
1000.00	438	+0.0002	51.338	+0.003	218.7	+0.000	2.782	+0.0000	-0.0000
2000.00	365	+0.0003	83.976	+0.003	222.6	+0.000	2.728	+0.0000	-0.0000
4000.00	303	+0.0003	137.439	+0.003	225.9	+0.000	2.693	+0.0000	-0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, E	Area-ratio exponent, n _E	Specific impulse, I _g (lb(lac)/lb)	Specific impulse exponent, n _I	Specific heat, C _p (cal/(g)(°K))	(∂ ln P / ∂ ln T) _T	(∂ ln P / ∂ ln T) _P
R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190									
1.00	1183	0.0000					1.7753	0.0000	0.0000
1.05	1168	+0.0000	2.250	0.0000	47.4	0.0000	1.7710	+0.0000	+0.0000
1.20	1129	+0.0000	1.297	+0.0000	90.8	+0.0000	1.7597	+0.0000	+0.0000
1.40	1085	+0.0000	1.081	+0.0000	122.2	+0.0000	1.7472	+0.0000	+0.0000
1.60	1049	+0.0000	1.018	+0.0000	143.2	+0.0000	1.7370	+0.0000	+0.0000
1.87	1008	+0.0000	1.000	+0.0000	163.4	+0.0000	1.7256	+0.0000	+0.0000
2.00	989	+0.0000	1.003	+0.0000	171.5	+0.0000	1.7210	+0.0000	+0.0000
4.00	824	+0.0000	1.233	+0.0000	232.3	+0.0000	1.6824	+0.0000	+0.0000
10.00	643	+0.0000	1.974	+0.0000	283.1	+0.0000	1.6506	+0.0000	+0.0000
20.00	532	+0.0000	2.983	+0.0000	309.9	+0.0000	1.6345	+0.0000	+0.0000
40.00	439	+0.0000	4.620	+0.0000	330.4	+0.0000	1.6269	+0.0000	+0.0000
40.83	437	+0.0000	4.682	+0.0000	330.9	+0.0000	1.6267	+0.0000	+0.0000
100.00	340	+0.0000	8.432	+0.0000	350.8	+0.0000	1.6089	+0.0000	+0.0000
200.00	280	+0.0000	13.431	+0.0000	362.6	+0.0000	1.5951	+0.0000	+0.0000
400.00	230	+0.0000	21.488	+0.0000	372.0	+0.0000	1.5558	+0.0000	+0.0000
1000.00	175	+0.0000	39.928	+0.0000	381.6	+0.0000	1.4852	+0.0000	+0.0000
2000.00	142	+0.0000	63.572	+0.0000	387.2	+0.0000	1.4387	+0.0000	+0.0000
4000.00	114	+0.0000	100.938	+0.0000	391.6	+0.0000	1.4039	+0.0000	+0.0000
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587									
1.00	1514	0.0000					1.6187	0.0000	0.0000
1.05	1497	+0.0000	2.233	0.0000	49.3	0.0000	1.6143	+0.0000	+0.0000
1.20	1450	+0.0000	1.289	+0.0000	94.6	+0.0000	1.6024	+0.0000	+0.0000
1.40	1398	+0.0000	1.077	+0.0000	127.4	+0.0000	1.5888	+0.0000	+0.0000
1.60	1354	+0.0000	1.016	+0.0000	149.4	+0.0000	1.5773	+0.0000	+0.0000
1.85	1307	+0.0000	1.000	+0.0000	169.2	+0.0000	1.5651	+0.0000	+0.0000
2.00	1282	+0.0000	1.004	+0.0000	175.1	+0.0000	1.5584	+0.0000	+0.0000
4.00	1079	+0.0000	1.244	+0.0000	243.2	+0.0000	1.5046	+0.0000	+0.0000
10.00	852	+0.0000	2.009	+0.0000	297.2	+0.0000	1.4516	+0.0000	+0.0000
20.00	709	+0.0000	3.049	+0.0000	325.9	+0.0000	1.4232	+0.0000	+0.0000
40.00	588	+0.0000	4.739	+0.0000	346.0	+0.0000	1.4066	+0.0000	+0.0000
40.83	585	+0.0000	4.802	+0.0000	346.6	+0.0000	1.4062	+0.0000	+0.0000
100.00	458	+0.0000	8.679	+0.0000	370.0	+0.0000	1.3916	+0.0000	+0.0000
200.00	379	+0.0000	13.870	+0.0000	382.7	+0.0000	1.3808	+0.0000	+0.0000
400.00	312	+0.0000	22.296	+0.0000	393.0	+0.0000	1.3684	+0.0000	+0.0000
1000.00	242	+0.0000	41.979	+0.0000	403.5	+0.0000	1.3402	+0.0000	+0.0000
2000.00	198	+0.0000	67.687	+0.0000	409.7	+0.0000	1.2976	+0.0000	+0.0000
4000.00	161	+0.0000	108.754	+0.0000	414.6	+0.0000	1.2543	+0.0000	+0.0000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984									
1.00	1817	0.0001					1.4998	0.0001	-0.0084
1.05	1797	+0.0001	2.218	0.0000	50.3	0.0000	1.4955	+0.0001	-0.0094
1.20	1745	+0.0001	1.283	+0.0000	96.6	+0.0000	1.4840	+0.0001	-0.0093
1.40	1686	+0.0000	1.073	+0.0000	130.1	+0.0000	1.4712	+0.0001	-0.0092
1.60	1636	+0.0000	1.015	+0.0000	152.7	+0.0000	1.4604	+0.0000	-0.0091
1.83	1587	+0.0000	1.000	+0.0000	171.8	+0.0000	1.4494	+0.0000	-0.0091
2.00	1555	+0.0000	1.005	+0.0000	183.1	+0.0000	1.4423	+0.0000	-0.0091
4.00	1322	+0.0000	1.256	+0.0000	249.3	+0.0000	1.3874	+0.0000	+0.0000
10.00	1057	+0.0000	2.048	+0.0000	305.6	+0.0000	1.3225	+0.0000	+0.0000
20.00	887	+0.0000	3.127	+0.0000	335.7	+0.0000	1.2849	+0.0000	+0.0000
40.00	741	+0.0000	4.883	+0.0000	359.0	+0.0000	1.2560	+0.0000	+0.0000
40.83	737	+0.0000	4.949	+0.0000	359.6	+0.0000	1.2552	+0.0000	+0.0000
100.00	581	+0.0000	8.985	+0.0000	382.4	+0.0000	1.2321	+0.0000	+0.0000
200.00	482	+0.0000	14.396	+0.0000	395.9	+0.0000	1.2189	+0.0000	+0.0000
400.00	399	+0.0000	23.208	+0.0000	406.8	+0.0000	1.2100	+0.0000	+0.0000
1000.00	310	+0.0000	43.893	+0.0000	418.1	+0.0000	1.1949	+0.0000	+0.0000
2000.00	256	+0.0000	71.279	+0.0000	424.7	+0.0000	1.1810	+0.0000	+0.0000
4000.00	210	+0.0000	115.650	+0.0000	430.2	+0.0000	1.1485	+0.0000	+0.0000
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381									
1.00	2094	0.0006					1.4145	0.00010	-0.0027
1.05	2073	+0.0005	2.206	0.0002	50.8	0.0002	1.4097	+0.00009	-0.0025
1.20	2016	+0.0004	1.277	+0.0001	97.5	+0.0002	1.3967	+0.00007	-0.0019
1.40	1952	+0.0003	1.071	+0.0001	131.4	+0.0002	1.3825	+0.00005	-0.0013
1.60	1898	+0.0002	1.013	+0.0000	154.2	+0.0001	1.3706	+0.00003	-0.0010
1.82	1847	+0.0001	1.000	+0.0000	172.7	+0.0001	1.3598	+0.00002	-0.0007
2.00	1809	+0.0001	1.006	+0.0000	185.1	+0.0001	1.3519	+0.00002	-0.0006
4.00	1553	+0.0000	1.266	+0.0001	252.6	+0.0001	1.2991	+0.00000	+0.0001
10.00	1257	+0.0000	2.085	+0.0001	310.4	+0.0000	1.2336	+0.00000	+0.0000
20.00	1064	+0.0001	3.206	+0.0000	341.7	+0.0000	1.1891	+0.00000	+0.0000
40.83	891	+0.0001	5.106	+0.0000	366.6	+0.0000	1.1522	+0.00000	+0.0000
40.00	895	+0.0001	5.037	+0.0000	366.0	+0.0000	1.1531	+0.00000	+0.0000
100.00	707	+0.0001	9.324	+0.0000	390.5	+0.0000	1.1174	+0.00000	+0.0000
200.00	590	+0.0001	14.993	+0.0000	404.8	+0.0000	1.1007	+0.00000	+0.0000
400.00	490	+0.0001	24.234	+0.0000	416.3	+0.0000	1.0867	+0.00000	+0.0000
1000.00	383	+0.0001	45.999	+0.0000	428.3	+0.0000	1.0746	+0.00000	+0.0000
2000.00	317	+0.0001	74.912	+0.0000	435.4	+0.0000	1.0638	+0.00000	+0.0000
4000.00	262	+0.0001	122.185	+0.0000	441.2	+0.0000	1.0534	+0.00000	+0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, E	Area-ratio exponent, n _E	Specific impulse, I (lb sec)/lb	Specific-impulse exponent, n _I	Specific heat, c _p (Btu/lb°K)	(∂ ln M / ∂ ln P) _T	(∂ ln M / ∂ ln T) _P
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778									
1.00	2347	0.0019	2.195	0.0007	50.9	0.0007	1.3691	0.00042	-0.0101
1.05	2325	.0018	2.173	.0005	97.7	.0007	1.3621	.00039	-.0093
1.20	2266	.0014	1.273	.0005	97.7	.0007	1.3440	.00030	-.0074
1.40	2198	.0010	1.068	.0003	131.8	.0006	1.3249	.00022	-.0057
1.60	2140	.0008	1.012	.0001	154.7	.0005	1.3099	.00017	-.0044
1.81	2089	.0006	1.000	.0000	172.5	.0005	1.2974	.00013	-.0035
2.00	2046	.0004	1.007	-.0001	185.9	.0004	1.2874	.00010	-.0028
4.00	1771	-.0001	1.275	-.0003	254.1	.0003	1.2291	.00002	-.0006
10.00	1451	-.0002	2.119	-.0003	313.0	.0001	1.1655	.00000	.0000
20.00	1238	-.0002	3.281	-.0003	345.1	.0001	1.1204	.00000	.0000
40.83	1045	-.0002	5.260	-.0003	370.9	.0001	1.0783	.00000	.0000
40.00	1050	-.0002	5.188	-.0003	370.3	.0001	1.0794	.00000	.0000
100.00	838	-.0002	9.676	-.0003	395.8	.0001	1.0365	.00000	.0000
200.00	702	-.0002	15.626	-.0002	416.8	.0000	1.0118	.00000	.0000
400.00	586	-.0002	25.350	-.0002	422.9	.0000	.9953	.00000	.0000
1000.00	460	-.0002	48.288	-.0002	435.5	.0000	.9789	.00000	.0000
2000.00	382	-.0002	78.852	-.0002	443.1	.0000	.9692	.00000	.0000
4000.00	317	-.0002	128.949	-.0002	445.2	.0000	.9590	.00000	.0000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175									
1.00	2574	0.0046	2.184	0.0014	50.7	0.0017	1.3697	0.00120	-0.0266
1.05	2552	.0043	2.168	.0010	97.5	.0016	1.3599	.00112	-.0250
1.20	2492	.0036	1.065	.0006	131.5	.0014	1.3344	.00091	-.0208
1.40	2422	.0028	1.011	.0002	154.5	.0013	1.3072	.00071	-.0167
1.60	2363	.0023	1.000	.0000	171.4	.0012	1.2856	.00057	-.0136
1.79	2313	.0018	1.008	-.0002	185.7	.0011	1.2685	.00047	-.0113
2.00	2266	.0015	1.008	-.0002	185.7	.0011	1.2533	.00038	-.0095
4.00	1978	.0001	1.284	-.0009	254.4	.0007	1.1787	.00009	-.0025
10.00	1637	-.0005	2.150	-.0011	314.1	.0004	1.1109	.00001	-.0003
20.00	1408	-.0005	3.351	-.0010	346.9	.0003	1.0669	.00000	.0000
40.00	1204	-.0006	5.334	-.0010	372.7	.0002	1.0253	.00000	.0000
40.83	1199	-.0006	5.409	-.0010	373.4	.0002	1.0242	.00000	.0000
100.00	970	-.0006	10.029	-.0009	399.1	.0002	.9767	.00000	.0000
200.00	818	-.0006	16.282	-.0009	414.7	.0001	.9478	.00000	.0000
400.00	687	-.0006	26.525	-.0009	427.4	.0001	.9249	.00000	.0000
1000.00	542	-.0006	50.761	-.0009	440.7	.0001	.9037	.00000	.0000
2000.00	452	-.0006	83.105	-.0009	448.6	.0001	.8928	.00000	.0000
4000.00	376	-.0006	136.261	-.0009	455.1	.0000	.8835	.00000	.0000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571									
1.00	2773	0.0085	2.172	0.0021	50.4	0.0031	1.4156	0.00266	-0.0555
1.05	2752	.0081	2.163	.0015	96.9	.0029	1.4027	.00251	-.0527
1.20	2692	.0070	1.063	.0009	130.8	.0027	1.3686	.00212	-.0455
1.40	2624	.0059	1.010	.0004	153.7	.0025	1.3318	.00174	-.0389
1.60	2565	.0047	1.000	.0000	169.6	.0023	1.3022	.00144	-.0322
1.78	2517	.0043	1.009	-.0004	184.9	.0022	1.2799	.00123	-.0280
2.00	2467	.0036	1.009	-.0004	184.9	.0022	1.2573	.00104	-.0240
4.00	2174	.0006	1.293	-.0020	253.7	.0015	1.1514	.00031	-.0081
10.00	1817	-.0008	2.182	-.0026	314.1	.0009	1.0682	.00004	-.0012
20.00	1575	-.0011	3.420	-.0025	347.4	.0007	1.0237	.00001	-.0002
40.00	1357	-.0012	5.476	-.0024	375.8	.0005	.9828	.00000	.0000
40.83	1350	-.0012	5.554	-.0024	374.5	.0005	.9816	.00000	.0000
100.00	1104	-.0012	10.381	-.0024	401.0	.0003	.9325	.00000	.0000
200.00	937	-.0013	16.950	-.0023	417.2	.0003	.8996	.00000	.0000
400.00	792	-.0013	27.755	-.0023	430.4	.0002	.8727	.00000	.0000
1000.00	629	-.0014	53.398	-.0023	444.3	.0002	.8465	.00000	.0000
2000.00	526	-.0014	87.714	-.0023	452.7	.0001	.8313	.00000	.0000
4000.00	439	-.0014	144.197	-.0023	459.5	.0001	.8210	.00000	.0000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968									
1.00	2944	0.0131	2.162	0.0026	50.0	0.0047	1.5012	0.00493	-0.0983
1.05	2923	.0127	2.158	.0019	96.1	.0044	1.4856	.00469	-.0943
1.20	2866	.0114	1.061	.0012	129.7	.0042	1.4440	.00409	-.0837
1.40	2800	.0099	1.010	.0005	152.5	.0039	1.3979	.00347	-.0723
1.60	2742	.0087	1.000	.0000	167.4	.0038	1.3600	.00298	-.0633
1.77	2699	.0078	1.000	.0000	167.4	.0038	1.3324	.00264	-.0588
2.00	2647	.0068	1.010	-.0006	183.5	.0036	1.3008	.00227	-.0497
4.00	2356	.0021	1.303	-.0032	252.4	.0026	1.1551	.00083	-.0202
10.00	1990	-.0010	2.216	-.0047	313.1	.0017	1.0408	.00015	-.0041
20.00	1737	-.0018	3.491	-.0049	346.9	.0014	.9888	.00003	-.0009
40.00	1507	-.0020	5.620	-.0048	373.8	.0009	.9482	.00000	-.0001
40.83	1501	-.0020	5.701	-.0048	374.5	.0009	.9471	.00000	-.0001
100.00	1238	-.0022	10.736	-.0047	401.7	.0007	.8984	.00000	.0000
200.00	1059	-.0023	17.634	-.0046	418.5	.0005	.8634	.00000	.0000
400.00	900	-.0023	29.032	-.0046	432.2	.0004	.8333	.00000	.0000
1000.00	720	-.0024	56.203	-.0046	446.7	.0003	.8013	.00000	.0000
2000.00	606	-.0023	92.675	-.0046	455.5	.0002	.7841	.00000	.0000
4000.00	507	-.0025	152.844	-.0046	462.7	.0002	.7696	.00000	.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, E	Area-ratio exponent, n _E	Specific impulse, I _{sp} (lb-sec/lb)	Specific-impulse exponent, n _I	Specific heat, c _p (cal/g-°K)	(∂ ln P / ∂ ln P) _T	(∂ ln P / ∂ ln T) _P
R = 3.60, PERCENT FUEL = 17.35, O/F = 4.762									
1.00	3208	0.0226					1.7671	0.01210	-0.2283
1.05	3189	0.0221	2.144	0.0028	48.8	0.0078	1.7482	0.01170	-0.2219
1.20	3137	0.0208	1.250	0.0021	93.8	0.0075	1.6966	0.01063	-0.2047
1.40	3077	0.0192	1.057	0.0013	126.8	0.0073	1.6375	0.00947	-0.1854
1.60	3025	0.0178	1.007	0.0005	149.1	0.0070	1.5869	0.00852	-0.1693
1.75	2990	0.0169	1.000	0.0000	162.3	0.0069	1.5531	0.00791	-0.1588
2.00	2938	0.0155	1.012	-0.0008	179.7	0.0066	1.5041	0.00705	-0.1438
4.00	2669	0.0083	1.323	-0.0048	248.0	0.0054	1.2723	0.00352	-0.0779
10.00	2313	0.0006	2.288	-0.0091	309.3	0.0039	1.0538	0.00101	-0.0253
20.00	2050	-0.0027	3.644	-0.0108	343.7	0.0030	0.9574	0.00029	-0.0081
40.00	1803	-0.0041	5.926	-0.0113	371.5	0.0023	0.8996	0.00006	-0.0019
40.83	1796	-0.0041	6.013	-0.0113	372.3	0.0023	0.8983	0.00006	-0.0019
100.00	1506	-0.0047	11.474	-0.0112	400.7	0.0017	0.8482	0.00000	-0.0002
200.00	1306	-0.0050	19.054	-0.0111	418.4	0.0013	0.8136	0.00000	0.0000
400.00	1125	-0.0052	31.724	-0.0110	433.1	0.0011	0.7807	0.00000	0.0000
1000.00	916	-0.0055	62.274	-0.0110	448.8	0.0008	0.7420	0.00000	0.0000
2000.00	778	-0.0056	103.640	-0.0111	458.4	0.0007	0.7177	0.00000	0.0000
4000.00	658	-0.0058	172.288	-0.0111	466.4	0.0005	0.6983	0.00000	0.0000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556									
1.00	3381	0.0307					2.1301	0.02284	-0.4169
1.05	3364	0.0303	2.133	0.0024	47.4	0.0105	2.1115	0.02230	-0.4091
1.20	3317	0.0291	1.245	0.0018	91.2	0.0101	2.0594	0.02089	-0.3876
1.40	3263	0.0278	1.054	0.0011	123.3	0.0098	1.9976	0.01921	-0.3628
1.60	3217	0.0266	1.006	0.0004	145.2	0.0096	1.9428	0.01783	-0.3412
1.75	3188	0.0258	1.000	0.0000	157.0	0.0095	1.9085	0.01699	-0.3280
2.00	3140	0.0245	1.014	-0.0007	175.1	0.0093	1.8496	0.01560	-0.3055
4.00	2903	0.0173	1.339	-0.0047	242.3	0.0084	1.5556	0.00954	-0.2008
10.00	2584	0.0070	2.356	-0.0106	303.3	0.0066	1.2090	0.00394	-0.0917
20.00	2337	0.0000	3.803	-0.0147	338.3	0.0054	1.0195	0.00159	-0.0403
40.00	2088	-0.0048	6.256	-0.0174	366.8	0.0043	0.9006	0.00050	-0.0139
40.83	2081	-0.0049	6.350	-0.0175	367.6	0.0043	0.8980	0.00048	-0.0135
100.00	1775	-0.0076	12.271	-0.0186	397.1	0.0032	0.8183	0.00007	-0.0023
200.00	1558	-0.0083	20.571	-0.0186	415.7	0.0026	0.7809	0.00001	-0.0004
400.00	1359	-0.0087	34.597	-0.0186	431.3	0.0021	0.7484	0.00000	-0.0001
1000.00	1175	-0.0093	68.879	-0.0186	448.2	0.0016	0.7080	0.00000	0.0000
2000.00	968	-0.0096	115.835	-0.0187	458.6	0.0013	0.6798	0.00000	0.0000
4000.00	828	-0.0100	194.445	-0.0188	467.4	0.0011	0.6552	0.00000	0.0000
R = 0.80, PERCENT FUEL = 13.60, O/F = 6.349									
1.00	3481	0.0364					2.4909	0.03537	-0.6319
1.05	3465	0.0361	2.126	0.0018	46.0	0.0119	2.4777	0.03482	-0.6249
1.20	3422	0.0352	1.262	0.0014	88.5	0.0118	2.4401	0.03330	-0.6052
1.40	3375	0.0341	1.052	0.0008	119.7	0.0116	2.3938	0.03195	-0.5818
1.60	3331	0.0332	1.006	0.0003	140.9	0.0114	2.3513	0.03003	-0.5609
1.75	3306	0.0326	1.000	0.0000	151.8	0.0113	2.3254	0.02915	-0.5485
2.00	3261	0.0316	1.015	-0.0009	170.0	0.0112	2.2752	0.02752	-0.5249
4.00	3052	0.0260	1.350	-0.0036	235.7	0.0103	2.0021	0.01991	-0.4058
10.00	2779	0.0170	2.409	-0.0088	296.0	0.0090	1.5823	0.01097	-0.2447
20.00	2568	0.0087	3.944	-0.0139	331.1	0.0080	1.2725	0.00579	-0.1390
40.00	2346	0.0000	6.587	-0.0192	360.1	0.0068	1.0267	0.00247	-0.0641
40.83	2340	-0.0002	6.689	-0.0194	360.8	0.0068	1.0207	0.00240	-0.0625
100.00	2042	-0.0083	13.134	-0.0243	391.4	0.0053	0.8369	0.00055	-0.0159
200.00	1815	-0.0113	22.231	-0.0256	410.6	0.0043	0.7683	0.00013	-0.0041
400.00	1602	-0.0126	37.727	-0.0261	427.3	0.0035	0.7287	0.00002	-0.0008
1000.00	1347	-0.0135	76.063	-0.0262	445.3	0.0027	0.6888	0.00000	-0.0001
2000.00	1173	-0.0141	129.237	-0.0263	456.6	0.0023	0.6594	0.00000	0.0000
4000.00	1016	-0.0147	219.200	-0.0265	466.2	0.0019	0.6320	0.00000	0.0000
R = 0.90, PERCENT FUEL = 12.28, O/F = 7.143									
1.00	3526	0.0393					2.6696	0.04460	-0.7874
1.05	3511	0.0390	2.123	0.0015	44.5	0.0127	2.6628	0.04411	-0.7823
1.20	3469	0.0383	1.241	0.0011	85.8	0.0126	2.6432	0.04279	-0.7680
1.40	3422	0.0374	1.052	0.0006	116.1	0.0125	2.6185	0.04126	-0.7508
1.60	3382	0.0367	1.005	0.0002	136.7	0.0123	2.5953	0.03994	-0.7355
1.75	3360	0.0362	1.000	0.0000	147.0	0.0123	2.5813	0.03918	-0.7265
2.00	3317	0.0354	1.016	-0.0005	165.0	0.0121	2.5526	0.03773	-0.7087
4.00	3122	0.0314	1.356	-0.0027	228.9	0.0114	2.3886	0.03089	-0.6170
10.00	2881	0.0254	2.437	-0.0061	287.9	0.0105	2.0940	0.02206	-0.4769
20.00	2705	0.0199	4.032	-0.0094	322.5	0.0098	1.8100	0.01550	-0.3584
40.00	2528	0.0127	6.838	-0.0138	351.5	0.0089	1.4813	0.00946	-0.2343
40.83	2523	0.0125	6.947	-0.0140	352.3	0.0089	1.4712	0.00930	-0.2309
100.00	2279	-0.0001	13.977	-0.0222	383.4	0.0076	1.0541	0.00335	-0.0922
200.00	2072	-0.0095	24.037	-0.0286	403.7	0.0065	0.8410	0.00105	-0.0315
400.00	1857	-0.0149	41.251	-0.0319	421.1	0.0055	0.7376	0.00025	-0.0080
1000.00	1585	-0.0176	84.153	-0.0331	440.3	0.0045	0.6784	0.00004	-0.0007
2000.00	1397	-0.0186	144.295	-0.0335	452.5	0.0036	0.6487	0.00000	-0.0001
4000.00	1224	-0.0194	247.166	-0.0335	463.0	0.0030	0.6217	0.00000	0.0000

TABLE III. - Continued. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRES-
SURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Continued. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P _c /P	Temperature, T, °K	Temperature exponent, n _T	Area ratio, E	Area ratio exponent, n _E	Specific impulse, I _{sp} (lb _m /sec)/lb	Specific impulse exponent, n _I	Specific heat, c _p (cal/(g ^o K))	(∂ ln P) _T	(∂ ln T) _P
R = 1.00, PERCENT FUEL = 11.19, O/F = 7.937									
1.00	3534	0.0399					2.6053	0.04709	-0.8301
1.05	3519	+0.296	2.122	0.0014	43.3	0.0129	2.6007	+0.4664	-0.8258
1.20	3478	+0.389	1.240	+0.010	83.3	+0.128	2.5874	+0.4541	-0.8135
1.40	3431	+0.381	1.051	+0.005	112.7	+0.126	2.5703	+0.4399	-0.7988
1.60	3392	+0.374	1.005	+0.002	132.7	+0.125	2.5542	+0.4277	-0.7857
1.73	3370	+0.370	1.000	+0.000	142.7	+0.124	2.5445	+0.4208	-0.7781
2.00	3327	+0.363	1.016	-0.004	160.1	+0.123	2.5243	+0.4073	-0.7630
4.70	3137	+0.327	1.357	-0.024	222.3	+0.117	2.4094	+0.3451	-0.6863
10.00	2903	+0.277	2.445	-0.053	279.6	+0.108	2.2079	+0.2666	-0.5732
20.00	2738	+0.256	4.055	-0.077	313.5	+0.102	2.0416	+0.2111	-0.4817
40.00	2578	+0.192	6.910	-0.103	341.7	+0.096	1.8120	+0.1600	-0.3879
40.83	2573	+0.190	7.022	-0.104	342.5	+0.095	1.8056	+0.1585	-0.3851
100.00	2371	+0.123	14.326	-0.146	373.2	+0.087	1.5117	+0.1011	-0.2667
200.00	2214	+0.061	25.124	-0.186	393.6	+0.080	1.2810	+0.0647	-0.1829
400.00	2052	-0.011	44.210	-0.235	411.4	+0.072	1.0654	+0.0366	-0.1117
1000.00	1826	-0.112	93.124	-0.305	431.8	+0.061	0.8338	+0.0132	-0.0452
2000.00	1648	-0.177	162.695	-0.352	445.0	+0.053	0.7163	+0.0047	-0.0177
4000.00	1470	-0.220	282.648	-0.381	456.5	+0.045	0.6444	+0.0013	-0.0053
R = 1.50, PERCENT FUEL = 7.76, O/F = 1.905									
1.00	3374	0.0324					1.6233	0.02714	-0.5145
1.20	3315	+0.312	1.242	0.0013	73.5	0.0107	1.5942	+0.2553	-0.4930
1.40	3258	+0.321	2.125	+0.017	38.2	+0.109	1.6157	+0.2671	-0.5088
1.60	3267	+0.302	1.052	+0.007	99.4	+0.106	1.5682	+0.2418	-0.4745
1.60	3226	+0.293	1.006	+0.003	117.1	+0.104	1.5447	+0.2304	-0.4583
1.73	3202	+0.288	1.000	+0.000	126.1	+0.103	1.5306	+0.2237	-0.4488
2.00	3158	+0.278	1.015	-0.005	141.3	+0.102	1.5034	+0.2115	-0.4308
4.70	2953	+0.250	1.351	-0.032	195.9	+0.094	1.3606	+0.1566	-0.3433
10.00	2692	+0.158	2.415	-0.073	246.1	+0.083	1.1474	+0.0942	-0.2294
20.00	2496	+0.097	3.967	-0.110	275.3	+0.074	0.9816	+0.0569	-0.1516
40.00	2297	+0.032	6.864	-0.151	299.5	+0.065	0.8274	+0.0298	-0.0879
40.83	2291	+0.030	6.788	-0.152	300.2	+0.065	0.8232	+0.0292	-0.0863
100.00	2026	-0.048	13.428	-0.204	325.0	+0.053	0.6842	+0.0095	-0.0328
200.00	1818	-0.091	22.891	-0.229	342.6	+0.044	0.5904	+0.0031	-0.0123
400.00	1616	-0.115	39.039	-0.243	356.7	+0.036	0.5432	+0.0008	-0.0037
1000.00	1366	-0.130	75.054	-0.249	372.3	+0.028	0.5048	+0.0001	-0.0005
2000.00	1193	-0.137	134.733	-0.251	382.1	+0.024	0.4834	+0.0000	-0.0001
4000.00	1039	-0.143	229.310	-0.253	390.4	+0.020	0.4636	+0.0000	-0.0000
R = 2.00, PERCENT FUEL = 5.92, O/F = 5.873									
1.00	3158	0.0243					1.1081	0.01418	-0.2964
1.05	3141	+0.240	2.132	0.0020	34.9	0.0086	1.1005	+0.1385	-0.2912
1.20	3097	+0.230	1.245	+0.015	67.1	+0.082	1.0794	+0.1296	-0.2770
1.40	3046	+0.219	1.054	+0.009	90.8	+0.083	1.0543	+0.1197	-0.2609
1.60	3002	+0.209	1.006	+0.003	106.9	+0.081	1.0320	+0.1114	-0.2465
1.74	2975	+0.203	1.000	+0.000	115.5	+0.080	1.0182	+0.1064	-0.2379
2.00	2929	+0.192	1.014	-0.006	128.9	+0.078	0.9940	+0.0980	-0.2232
4.70	2706	+0.157	1.341	-0.037	176.4	+0.069	0.8720	+0.0619	-0.1546
10.00	2413	+0.061	2.365	-0.083	223.5	+0.056	0.7166	+0.0278	-0.0797
20.00	2189	+0.009	3.829	-0.115	249.4	+0.047	0.6182	+0.0125	-0.0405
40.00	1965	-0.032	6.321	-0.140	270.5	+0.038	0.5459	+0.0046	-0.0170
40.83	1959	-0.033	6.416	-0.141	271.1	+0.038	0.5441	+0.0045	-0.0166
100.00	1678	-0.062	12.437	-0.156	293.1	+0.029	0.4875	+0.0009	-0.0039
200.00	1475	-0.072	20.879	-0.160	307.0	+0.023	0.4613	+0.0002	-0.0010
400.00	1289	-0.076	35.155	-0.160	318.7	+0.019	0.4417	+0.0000	-0.0002
1000.00	1070	-0.081	70.143	-0.160	331.3	+0.014	0.4194	+0.0000	-0.0000
2000.00	923	-0.084	118.235	-0.161	335.2	+0.012	0.4040	+0.0000	-0.0000
4000.00	792	-0.087	199.011	-0.162	345.8	+0.010	0.3894	+0.0000	-0.0000
R = 3.00, PERCENT FUEL = 4.03, O/F = 3.810									
1.00	2747	0.0120					0.6509	0.00385	-0.0973
1.05	2729	+0.117	2.152	0.0022	30.6	0.0046	0.6451	+0.0369	-0.0940
1.20	2679	+0.107	1.254	+0.016	58.8	+0.044	0.6293	+0.0328	-0.0853
1.40	2622	+0.096	1.058	+0.009	79.4	+0.042	0.6114	+0.0284	-0.0758
1.60	2573	+0.086	1.008	+0.004	93.4	+0.040	0.5966	+0.0249	-0.0680
1.75	2538	+0.079	1.000	+0.000	102.1	+0.039	0.5838	+0.0226	-0.0628
2.00	2491	+0.071	1.011	-0.005	114.5	+0.037	0.5720	+0.0197	-0.0561
4.70	2237	+0.029	1.314	-0.030	155.0	+0.029	0.5059	+0.0085	-0.0275
10.00	1913	-0.005	2.253	-0.050	192.9	+0.020	0.4460	+0.0021	-0.0089
20.00	1682	-0.017	3.569	-0.055	214.0	+0.015	0.4185	+0.0005	-0.0025
40.00	1470	-0.022	5.778	-0.056	231.0	+0.011	0.4000	+0.0001	-0.0006
40.83	1464	-0.022	5.862	-0.056	231.4	+0.011	0.3995	+0.0001	-0.0006
100.00	1220	-0.024	11.130	-0.055	248.7	+0.008	0.3811	+0.0000	-0.0001
200.00	1053	-0.025	18.422	-0.055	259.4	+0.006	0.3679	+0.0000	-0.0000
400.00	904	-0.026	30.593	-0.054	268.3	+0.005	0.3555	+0.0000	-0.0000
1000.00	733	-0.027	59.908	-0.054	277.8	+0.004	0.3398	+0.0000	-0.0000
2000.00	622	-0.028	99.549	-0.054	283.5	+0.003	0.3290	+0.0000	-0.0000
4000.00	525	-0.029	165.173	-0.055	286.3	+0.003	0.3194	+0.0000	-0.0000

TABLE III. - Concluded. THERMODYNAMIC DERIVATIVES AT ASSIGNED PRESSURE RATIOS FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

[Equilibrium composition during isentropic expansion. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute

Pressure ratio, P_c/P	Temperature, T, °K	Temperature exponent, n_T	Area ratio, a	Area-ratio exponent, n_a	Specific impulse, I, (lb)(sec)/lb	Specific-impulse exponent, n_I	Specific heat, C_p , cal/(g)(°K)	$(\frac{\partial \ln \eta}{\partial \ln P})_T$	$(\frac{\partial \ln \eta}{\partial \ln T})_P$
R = 4.00, PERCENT FUEL = 3.05, C/F = 1.746									
1.00	2381	0.0046			27.6	0.0019	0.4697	0.00095	-0.0288
1.05	2362	-0.0044	2.174	0.0013	53.0	-0.0017	0.4663	0.00089	-0.0274
1.20	2309	-0.0038	1.263	-0.0009	71.5	-0.0016	0.4572	0.00075	-0.0235
1.40	2249	-0.0031	1.063	-0.0005	84.0	-0.0015	0.4473	0.00060	-0.0196
1.60	2198	-0.0026	1.010	-0.0002	92.8	-0.0014	0.4393	0.00050	-0.0166
1.78	2157	-0.0022	1.000	-0.0000	101.1	-0.0013	0.4332	0.00042	-0.0145
2.00	2113	-0.0018	1.009	-0.0002	138.7	-0.0039	0.4272	0.00035	-0.0124
4.00	1860	-0.0003	1.293	-0.0011	171.6	0.0035	0.3982	0.00011	-0.0044
10.00	1554	-0.0005	2.182	-0.0015	189.8	0.0034	0.3743	0.00002	-0.0008
20.00	1348	-0.0006	3.423	-0.0015	204.3	0.0033	0.3612	0.00000	-0.0002
40.00	1164	-0.0007	5.493	-0.0014	204.7	0.0033	0.3499	0.00000	0.0000
40.83	1159	-0.0007	5.572	-0.0014	204.7	0.0033	0.3495	0.00000	0.0000
100.00	952	-0.0007	10.461	-0.0014	215.2	0.0002	0.3352	0.00000	0.0000
200.00	813	-0.0007	17.162	-0.0013	228.2	0.0002	0.3243	0.00000	0.0000
400.00	690	-0.0008	28.237	-0.0013	235.5	0.0001	0.3139	0.00000	0.0000
1000.00	551	-0.0008	54.608	-0.0013	243.3	0.0001	0.3012	0.00000	0.0000
2000.00	463	-0.0008	89.893	-0.0013	247.9	0.0001	0.2927	0.00000	0.0000
4000.00	386	-0.0008	147.835	-0.0013	251.8	0.0001	0.2864	0.00000	0.0000
R = 5.00, PERCENT FUEL = 2.45, C/F = 9.683									
1.00	2072	0.0015			25.2	0.0006	0.3924	0.00022	-0.0080
1.05	2053	-0.0014	2.190	0.0005	48.5	-0.0006	0.3906	0.00020	-0.0074
1.20	2002	-0.0011	1.270	-0.0004	65.4	-0.0006	0.3859	0.00016	-0.0061
1.40	1944	-0.0008	1.067	-0.0002	76.8	-0.0004	0.3808	0.00012	-0.0049
1.60	1894	-0.0007	1.011	-0.0001	85.3	-0.0004	0.3767	0.00010	-0.0038
1.80	1852	-0.0005	1.000	-0.0000	92.3	-0.0004	0.3734	0.00008	-0.0032
2.00	1813	-0.0004	1.007	-0.0001	126.2	0.0004	0.3706	0.00006	-0.0026
4.00	1578	0.0000	1.281	-0.0003	155.8	0.0001	0.3559	0.00001	-0.0007
10.00	1303	-0.0002	2.143	-0.0003	172.0	0.0001	0.3410	0.00000	-0.0001
20.00	1122	-0.0002	3.341	-0.0003	184.7	0.0001	0.3309	0.00000	0.0000
40.00	961	-0.0002	5.329	-0.0003	185.1	0.0001	0.3209	0.00000	0.0000
40.83	956	-0.0002	5.405	-0.0003	185.1	0.0001	0.3206	0.00000	0.0000
100.00	777	-0.0002	10.063	-0.0003	197.9	0.0000	0.3076	0.00000	0.0000
200.00	658	-0.0002	16.396	-0.0003	209.7	0.0000	0.2979	0.00000	0.0000
400.00	554	-0.0002	26.787	-0.0003	212.0	0.0000	0.2887	0.00000	0.0000
1000.00	438	-0.0002	51.327	-0.0003	218.7	0.0000	0.2782	0.00000	0.0000
2000.00	365	-0.0002	83.959	-0.0003	222.6	0.0000	0.2728	0.00000	0.0000
4000.00	303	-0.0002	137.411	-0.0003	225.9	0.0000	0.2693	0.00000	0.0000

TABLE IV. - EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN

AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Combustion-chamber pressure, 60 pounds per square inch absolute

R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	32.17	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	1183	1129	1035	1049	1008	824	819	643	532	459	340	260	175	142
H ₂	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000
H ₂ O	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	32.44	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	1514	1450	1398	1354	1307	1079	1073	852	709	588	458	379	242	198
H	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.79999	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000
H ₂ O	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	32.78	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	1816	1744	1666	1636	1567	1322	1316	1057	887	741	581	482	310	226
H	0.00017	0.00010	0.00006	0.00004	0.00003	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.74985	.74991	.74994	.74996	.74998	.75000	.75000	.75000	.75000	.75000	.75000	.75000	.75000	.75000
H ₂ O	.24997	.24998	.24999	.24999	.24999	.25000	.25000	.25000	.25000	.25000	.25000	.25000	.25000	.25000
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	33.04	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	2089	2013	1950	1896	1846	1553	1546	1258	1064	896	708	599	383	271
H	0.00120	0.00080	0.00056	0.00040	0.00029	0.00003	0.00003	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.63899	.63932	.63953	.63966	.63976	.63998	.63998	.63998	.63999	.63999	.63999	.63999	.63999	.63999
H ₂ O	.29975	.29984	.29989	.29992	.29995	.30000	.30000	.30000	.30000	.30000	.30000	.30000	.30000	.30000
OH	.00066	.00064	.00062	.00061	.00061	.00060	.00060	.00060	.00060	.00060	.00060	.00060	.00060	.00060
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	33.32	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	2329	2253	2189	2135	2085	1772	1764	1452	1239	1051	838	703	460	382
H	0.00446	0.00328	0.00248	0.00192	0.00151	0.00022	0.00021	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.64640	.64735	.64799	.64844	.64877	.64962	.64983	.64999	.64999	.64999	.64999	.64999	.64999	.64999
H ₂ O	.34873	.34910	.34946	.34971	.34986	.34995	.34999	.34999	.34999	.34999	.34999	.34999	.34999	.34999
OH	.00041	.00027	.00019	.00013	.00010	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	33.62	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	2531	2458	2395	2342	2298	1978	1970	1640	1411	1207	972	820	543	453
H	0.01092	0.00867	0.00702	0.00577	0.00488	0.00106	0.00102	0.00010	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000
O	.20002	.20001	.20001	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000
H ₂	.59160	.59331	.59456	.59552	.59621	.59916	.59920	.59992	.59999	.59999	.59999	.59999	.59999	.59999
H ₂ O	.39584	.39583	.39752	.39802	.39837	.39970	.39972	.39998	.39999	.39999	.39999	.39999	.39999	.39999
O ₂	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00161	.00118	.00088	.00068	.00054	.00007	.00007	.00000	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	33.93	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	2695	2628	2570	2519	2481	2167	2159	1822	1581	1362	1109	942	652	529
H	0.02018	0.01699	0.01451	0.01253	0.01115	0.00340	0.00328	0.00050	0.00007	0.00001	0.00000	0.00000	0.00000	0.00000
O	.00010	.00007	.00005	.00003	.00003	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H ₂	.53544	.53767	.53942	.54095	.54181	.54745	.54754	.54962	.54994	.54999	.54999	.54999	.54999	.54999
H ₂ O	.43989	.44183	.44326	.44438	.44507	.44877	.44882	.44983	.44998	.44999	.44999	.44999	.44999	.44999
O ₂	.00003	.00002	.00002	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00435	.00342	.00275	.00224	.00191	.00038	.00036	.00003	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	34.19	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	2828	2765	2707	2654	2632	2335	2327	1996	1748	1518	1247	1067	727	611
H	0.03077	0.02704	0.02422	0.02151	0.01985	0.00801	0.00779	0.00174	0.00035	0.00005	0.00000	0.00000	0.00000	0.00000
O	.30036	.30026	.30020	.30015	.30013	.30002	.30001	.30000	.30000	.30000	.30000	.30000	.30000	.30000
H ₂	.47961	.48192	.48302	.48395	.48468	.48930	.48931	.49174	.49174	.49199	.49199	.49199	.49199	.49199
H ₂ O	.47995	.48307	.48546	.48736	.48828	.49211	.49211	.49353	.49354	.49388	.49399	.49399	.49399	.49399
O ₂	.00015	.00011	.00008	.00006	.00005	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00915	.00760	.00642	.00550	.00491	.00140	.00134	.00018	.00002	.00000	.00000	.00000	.00000	.00000
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	34.55	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	3019	2961	2914	2874	2849	2559	2550	2229	2003	1829	1569	1329	922	792
H	0.04998	0.04628	0.04316	0.04048	0.03884	0.02303	0.02267	0.00943	0.00343	0.00087	0.00008	0.00001	0.00000	0.00000
O	.20207	.20167	.20141	.20121	.20109	.20003	.20003	.20000	.20000	.20000	.20000	.20000	.20000	.20000
H ₂	.37569	.37696	.37807	.37911	.37972	.38883	.38701	.39416	.39776	.39942	.39995	.39999	.39999	.39999
H ₂ O	.54591	.54580	.54598	.54622	.54644	.58144	.58162	.59399	.59681	.59962	.59997	.59999	.59999	.59999
O ₂	.00119	.00100	.00085	.00073	.00066	.00019	.00019	.00002	.00000	.00000	.00000	.00000	.00000	.00000
OH	.02520	.02250	.02031	.01849	.01741	.00819	.00801	.00235	.00059	.00009	.00000	.00000	.00000	.00000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556														
Pressure, lb/sq in. abs	60.00	50.00	42.86	37.50	34.75	15.00	14.70	6.00	3.00	1.50	0.60	0.30	0.06	0.03
Temperature, °K	3128	3078	3037	3001	2981	2761	2756	2517	2320	2106	1815	1596	1156	1033
H	0.06925	0.06590	0.06332	0.06135	0.06030	0.03770	0.03735	0.02275	0.01282	0.00559	0.00108	0.00020	0.00000	0.00000
O	.20590	.20525	.20473	.20429	.20406	.20192	.20188	.20008	.20015	.20002	.20000	.20000	.20000	.20000
H ₂	.28527	.28669	.28755	.28825	.28862	.29614	.29610	.29308	.29361	.29400	.29400	.29400	.29400	.29400
H ₂ O	.59195	.59164	.59165	.59173	.59175	.64882	.64702	.67400	.68717	.69579	.69936	.69991	.69999	.69999
O ₂	.00438	.00441	.00442	.00437	.00435	.00177	.00174	.00056	.00002	.00000	.00000	.00000	.00000	.00000
OH	.04705	.04376	.04101	.03867	.03735	.02366	.02335	.01147	.00511	.00161	.00018	.00002	.00000	.00000

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(a) Concluded. Combustion-chamber pressure, 60 pounds per square inch absolute

Table with 13 columns for pressure and temperature (60.00 to 0.03 lb/sq in. abs, 3100 to 1400 °K) and 13 rows for chemical species (H, O, H2, H2O, O2, OH). Each cell contains a mole fraction value. Sub-headers indicate R and U/F ratios for each section.

ETCC

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Combustion-chamber pressure, 150 pounds per square inch absolute

R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	80.42	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	1183	1129	1083	1049	1008	824	643	639	532	439	340	280	175	142
H ₂	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000
H ₂ O	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000	.15000
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	81.24	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	1514	1450	1398	1354	1307	1079	552	847	709	588	458	379	242	198
H	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.79999	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000	.80000
H ₂ O	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000	.20000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	81.96	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	1816	1745	1686	1636	1587	1350	1057	1052	887	741	581	482	310	256
H	0.00011	0.00007	0.00004	0.00003	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.74999	.74994	.74996	.74998	.74998	.75000	.75000	.75000	.75000	.75000	.75000	.75000	.75000	.75000
H ₂ O	.24998	.24999	.24999	.25000	.25000	.25000	.25000	.25000	.25000	.25000	.25000	.25000	.25000	.25000
R = 0.30, PERCENT FUEL = 29.57, O/F = 2.381														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	82.58	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2092	2015	1951	1897	1846	1553	1258	1251	1064	895	708	590	383	317
H	0.00077	0.00051	0.00036	0.00026	0.00018	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.69935	.69957	.69970	.69978	.69984	.69999	.70000	.70000	.70000	.70000	.70000	.70000	.70000	.70000
H ₂ O	.29984	.29990	.29993	.29995	.29997	.30000	.30000	.30000	.30000	.30000	.30000	.30000	.30000	.30000
OH	.00004	.00002	.00001	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	83.19	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2339	2259	2193	2137	2087	1772	1451	1444	1239	1051	838	702	460	382
H	0.00296	0.00215	0.00161	0.00124	0.00097	0.00014	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	.64761	.64826	.64869	.64899	.64921	.64988	.64999	.64999	.65000	.65000	.65000	.65000	.65000	.65000
H ₂ O	.34915	.34941	.34957	.34968	.34976	.34997	.35000	.35000	.35000	.35000	.35000	.35000	.35000	.35000
OH	.00028	.00018	.00012	.00009	.00006	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	83.84	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2553	2475	2410	2353	2306	1978	1638	1631	1410	1206	971	819	543	452
H	0.00758	0.00593	0.00474	0.00386	0.00322	0.00067	0.00006	0.00006	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000
O	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H ₂	.59418	.59543	.59633	.59701	.59750	.59947	.59995	.59995	.60000	.60000	.60000	.60000	.60000	.60000
H ₂ O	.39709	.39782	.39832	.39867	.39892	.39981	.39999	.39999	.40000	.40000	.40000	.40000	.40000	.40000
OH	.00115	.00082	.00061	.00046	.00036	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	84.52	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2733	2659	2590	2542	2499	2171	1819	1812	1578	1357	1106	939	631	528
H	0.01469	0.01217	0.01025	0.00875	0.00768	0.00220	0.00031	0.00029	0.00004	0.00000	0.00000	0.00000	0.00000	0.00000
O	.00006	.00004	.00003	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H ₂	.59341	.59417	.59453	.59480	.59486	.59485	.59477	.59478	.59497	.59500	.59500	.59500	.59500	.59500
H ₂ O	.44255	.44408	.44520	.44603	.44660	.44920	.44991	.44999	.45000	.45000	.45000	.45000	.45000	.45000
O ₂	.00002	.00001	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00328	.00253	.00199	.00160	.00134	.00025	.00002	.00002	.00000	.00000	.00000	.00000	.00000	.00000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	85.15	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2881	2811	2752	2701	2664	2346	1994	1986	1743	1512	1242	1063	724	608
H	0.02339	0.02026	0.01776	0.01573	0.01434	0.00537	0.00108	0.00104	0.00021	0.00003	0.00000	0.00000	0.00000	0.00000
O	.00021	.00015	.00011	.00008	.00007	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H ₂	.64852	.64866	.64884	.64894	.64904	.64924	.64922	.64923	.64964	.64998	.65000	.65000	.65000	.65000
H ₂ O	.48452	.48713	.48911	.49080	.49187	.49746	.49929	.49981	.49993	.49999	.50000	.50000	.50000	.50000
O ₂	.00009	.00006	.00005	.00003	.00003	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00727	.00594	.00493	.00416	.00366	.00095	.00011	.00010	.00001	.00000	.00000	.00000	.00000	.00000
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	86.09	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3097	3036	2980	2940	2911	2630	2208	2200	1938	1615	1318	1137	794	786
H	0.04050	0.03714	0.03433	0.03194	0.03042	0.01688	0.00625	0.00605	0.00211	0.00051	0.00004	0.00000	0.00000	0.00000
O	.00139	.00113	.00093	.00078	.00067	.00079	.00082	.00082	.00080	.00080	.00080	.00080	.00080	.00080
H ₂	.38933	.39124	.39257	.39331	.39342	.39335	.39335	.39363	.39864	.39956	.39997	.40000	.40000	.40000
H ₂ O	.59244	.59802	.59940	.60076	.60209	.60827	.60903	.60940	.60999	.60999	.60999	.60999	.60999	.60999
O ₂	.00082	.00067	.00056	.00047	.00042	.00011	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000
OH	.02181	.01923	.01716	.01540	.01440	.00623	.00157	.00152	.00036	.00003	.00000	.00000	.00000	.00000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.255														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	86.86	37.50	15.00	14.70	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3234	3176	3120	3077	3048	2823	2400	2394	2031	1702	1402	1209	844	793
H	0.05151	0.04846	0.04585	0.04394	0.04273	0.02990	0.01654	0.01631	0.00537	0.00157	0.00039	0.00010	0.00000	0.00000
O	.00334	.00294	.00255	.00224	.00200	.00228	.00232	.00232	.00230	.00230	.00230	.00230	.00230	.00230
H ₂	.36991	.37091	.37203	.37305	.37395	.37948	.38048	.38048	.38276	.38815	.39065	.39294	.39500	.39500
H ₂ O	.60391	.61347	.61971	.62490	.62929	.63929	.64504	.64504	.64919	.65147	.65267	.65299	.65300	.65300
O ₂	.00075	.00063	.00053	.00044	.00039	.00017	.00003	.00003	.00001	.00000	.00000	.00000	.00000	.00000
OH	.04323	.03983	.03711	.03475	.03280	.01795	.00672	.00692	.00348	.00097	.00029	.00004	.00000	.00000

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR

LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions.
Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(b) Concluded. Combustion-chamber pressure, 150 pounds per square inch absolute

R = 0.80, PERCENT FUEL = 13.6%, O/F = 6.349														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	86.97	81.50	75.00	67.50	7.50	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3304	3253	3211	3174	3154	3130	3104	3079	3052	3028	3004	2980	1375	1199
H	0.05409	0.05174	0.04977	0.04807	0.04712	0.04661	0.04632	0.04620	0.04617	0.04614	0.04612	0.04612	0.04612	0.04612
O	0.00948	0.00870	0.00806	0.00752	0.00723	0.00711	0.00703	0.00700	0.00700	0.00700	0.00700	0.00700	0.00700	0.00700
H ₂	0.22134	0.21952	0.21800	0.21669	0.21597	0.21562	0.21541	0.21531	0.21530	0.21530	0.21530	0.21530	0.21530	0.21530
H ₂ O	0.63789	0.64703	0.65470	0.66128	0.66645	0.67057	0.67361	0.67591	0.67754	0.67853	0.67903	0.67927	0.67931	0.67933
O ₂	0.01095	0.01030	0.00973	0.00925	0.00897	0.00881	0.00873	0.00870	0.00870	0.00870	0.00870	0.00870	0.00870	0.00870
OH	0.06624	0.06271	0.05974	0.05719	0.05577	0.05503	0.05451	0.05417	0.05395	0.05382	0.05376	0.05374	0.05374	0.05374
R = 0.90, PERCENT FUEL = 12.2%, O/F = 7.143														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	87.09	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3336	3286	3246	3211	3192	3167	3143	3119	3095	3072	3049	3026	1426	1247
H	0.05120	0.04913	0.04740	0.04592	0.04510	0.04461	0.04432	0.04419	0.04414	0.04412	0.04412	0.04412	0.04412	0.04412
O	0.01521	0.01428	0.01351	0.01287	0.01252	0.01238	0.01232	0.01230	0.01230	0.01230	0.01230	0.01230	0.01230	0.01230
H ₂	0.16900	0.16643	0.16418	0.16222	0.16113	0.16031	0.15981	0.15951	0.15941	0.15940	0.15940	0.15940	0.15940	0.15940
H ₂ O	0.65494	0.66481	0.67331	0.68031	0.68627	0.69093	0.69457	0.69725	0.69907	0.69993	0.70003	0.70003	0.70003	0.70003
O ₂	0.02360	0.02289	0.02226	0.02171	0.02140	0.02129	0.02127	0.02127	0.02127	0.02127	0.02127	0.02127	0.02127	0.02127
OH	0.08600	0.08247	0.07952	0.07697	0.07558	0.07502	0.07457	0.07424	0.07402	0.07391	0.07386	0.07386	0.07386	0.07386
R = 1.00, PERCENT FUEL = 11.1%, O/F = 7.937														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	87.13	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3341	3292	3252	3217	3199	3174	3150	3126	3102	3079	3056	3033	1450	1268
H	0.04560	0.04368	0.04207	0.04069	0.03994	0.03968	0.03962	0.03962	0.03962	0.03962	0.03962	0.03962	0.03962	0.03962
O	0.02044	0.01940	0.01854	0.01781	0.01741	0.01726	0.01722	0.01722	0.01722	0.01722	0.01722	0.01722	0.01722	0.01722
H ₂	0.13070	0.12776	0.12526	0.12306	0.12186	0.12109	0.12059	0.12029	0.12017	0.12012	0.12012	0.12012	0.12012	0.12012
H ₂ O	0.66145	0.67146	0.67991	0.68721	0.69281	0.69651	0.69891	0.70021	0.70081	0.70101	0.70101	0.70101	0.70101	0.70101
O ₂	0.04143	0.04030	0.03947	0.03874	0.03824	0.03794	0.03782	0.03782	0.03782	0.03782	0.03782	0.03782	0.03782	0.03782
OH	0.10038	0.09681	0.09332	0.09012	0.08842	0.08802	0.08782	0.08772	0.08772	0.08772	0.08772	0.08772	0.08772	0.08772
R = 1.50, PERCENT FUEL = 7.74, O/F = 1.905														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	86.98	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3219	3169	3127	3091	3071	3053	3026	2999	2974	2953	2931	2908	1393	1220
H	0.01925	0.01792	0.01683	0.01591	0.01540	0.01517	0.01505	0.01505	0.01505	0.01505	0.01505	0.01505	0.01505	0.01505
O	0.02906	0.02743	0.02607	0.02491	0.02427	0.02400	0.02387	0.02387	0.02387	0.02387	0.02387	0.02387	0.02387	0.02387
H ₂	0.04359	0.04143	0.03981	0.03805	0.03718	0.03659	0.03624	0.03612	0.03612	0.03612	0.03612	0.03612	0.03612	0.03612
H ₂ O	0.62812	0.63846	0.64580	0.65196	0.65621	0.65901	0.66071	0.66162	0.66192	0.66202	0.66202	0.66202	0.66202	0.66202
O ₂	0.06847	0.06585	0.06321	0.06057	0.05892	0.05805	0.05746	0.05706	0.05684	0.05674	0.05674	0.05674	0.05674	0.05674
OH	0.11152	0.10693	0.10306	0.09972	0.09785	0.09718	0.09662	0.09624	0.09599	0.09586	0.09586	0.09586	0.09586	0.09586
R = 2.00, PERCENT FUEL = 5.92, O/F = 5.873														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	86.67	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	3045	2992	2947	2909	2886	2864	2838	2814	2790	2764	2739	2714	1384	1204
H	0.00745	0.00667	0.00604	0.00552	0.00523	0.00503	0.00491	0.00491	0.00491	0.00491	0.00491	0.00491	0.00491	0.00491
O	0.02225	0.02043	0.01893	0.01767	0.01694	0.01659	0.01643	0.01643	0.01643	0.01643	0.01643	0.01643	0.01643	0.01643
H ₂	0.01742	0.01608	0.01497	0.01403	0.01348	0.01318	0.01303	0.01303	0.01303	0.01303	0.01303	0.01303	0.01303	0.01303
H ₂ O	0.57080	0.57738	0.58265	0.58746	0.59175	0.59518	0.59752	0.59892	0.59942	0.59962	0.59962	0.59962	0.59962	0.59962
O ₂	0.29542	0.29169	0.28794	0.28319	0.27746	0.27192	0.26664	0.26174	0.25724	0.25314	0.24944	0.24614	0.24324	0.24074
OH	0.08666	0.08157	0.07730	0.07303	0.06974	0.06718	0.06524	0.06384	0.06294	0.06244	0.06214	0.06204	0.06204	0.06204
R = 3.00, PERCENT FUEL = 4.03, O/F = 3.810														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	85.58	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2695	2634	2582	2537	2517	2500	2474	2450	2426	2402	2378	2354	1376	1204
H	0.00096	0.00077	0.00062	0.00051	0.00045	0.00040	0.00037	0.00037	0.00037	0.00037	0.00037	0.00037	0.00037	0.00037
O	0.00762	0.00641	0.00549	0.00475	0.00429	0.00399	0.00382	0.00382	0.00382	0.00382	0.00382	0.00382	0.00382	0.00382
H ₂	0.00307	0.00260	0.00224	0.00195	0.00176	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165	0.00165
H ₂ O	0.46923	0.47297	0.47594	0.47837	0.47995	0.48117	0.48197	0.48247	0.48287	0.48307	0.48307	0.48307	0.48307	0.48307
O ₂	0.48042	0.48284	0.48470	0.48622	0.48734	0.48794	0.48834	0.48864	0.48884	0.48894	0.48894	0.48894	0.48894	0.48894
OH	0.03870	0.03441	0.03096	0.02809	0.02621	0.02526	0.02466	0.02426	0.02396	0.02376	0.02366	0.02366	0.02366	0.02366
R = 4.00, PERCENT FUEL = 3.05, O/F = 1.746														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	84.31	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2383	2295	2238	2180	2149	2129	2103	2079	2054	2029	2004	1979	1452	1284
H	0.00009	0.00006	0.00004	0.00003	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002	0.00002
O	0.01619	0.01266	0.00997	0.00776	0.00618	0.00510	0.00430	0.00370	0.00320	0.00280	0.00240	0.00210	0.00180	0.00160
H ₂	0.00047	0.00035	0.00027	0.00022	0.00018	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016	0.00016
H ₂ O	0.39096	0.39265	0.39389	0.39464	0.39514	0.39544	0.39564	0.39574	0.39584	0.39594	0.39594	0.39594	0.39594	0.39594
O ₂	0.59335	0.59463	0.59557	0.59620	0.59660	0.59680	0.59690	0.59696	0.59706	0.59716	0.59716	0.59716	0.59716	0.59716
OH	0.01343	0.01105	0.00926	0.00787	0.00688	0.00618	0.00568	0.00528	0.00498	0.00478	0.00468	0.00468	0.00468	0.00468
R = 5.00, PERCENT FUEL = 2.45, O/F = 0.683														
Pressure, lb/sq in. abs	150.00	125.00	107.14	93.75	83.45	81.50	75.00	67.50	6.70	3.75	1.50	0.75	0.15	0.08
Temperature, °K	2066	1998	1941	1892	1870	1850	1824	1800	1776	1751	1726	1701	1438	1284
H	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
O	0.00028	0.00018	0.00013	0.00009	0.00007	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006	0.00006
H ₂	0.00006	0.00004	0.00003	0.00002	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001	0.00001
H ₂ O	0.33094	0.33154	0.33194	0.33222	0.33243	0.33253	0.33258	0.33262	0.33266	0.33268	0.33269	0.33269	0.33269	0.33269
O ₂	0.66482	0.66529	0.66561	0.66583	0.66594	0.66604	0.66609	0.66613	0.66616	0.66618	0.66619	0.66619	0.66619	0.66619
OH	0.00389	0.00295	0.00230	0.00183	0.00149	0.00133	0.00123	0.00118	0.00113	0.00108	0.00103	0.00103	0.00103	0.00103

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Combustion-chamber pressure, 300 pounds per square inch absolute

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Table with 15 columns for R values (0.15 to 0.70) and 15 rows for properties (Pressure, Temperature, H2, H2O, H, O, OH). Each cell contains numerical values for mole fractions and physical properties.

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(c) Concluded. Combustion-chamber pressure, 300 pounds per square inch absolute

Table with 15 columns of pressure and temperature data, and rows for chemical species (H, O, H2, H2O, O2, OH) across various R and O/F ratios (0.80, 0.90, 1.00, 1.50, 2.00, 3.00, 4.00, 5.00).

CONTINUED

TABLE IV. - Continued. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

(Isentropic expansion from chamber conditions; compositions are given in mole fractions. Equivalence ratio, R; oxidant-fuel ratio, O/F.)

(d) Combustion-chamber pressure, 600 pounds per square inch absolute

R = 0.15, PERCENT FUEL = 45.65, O/F = 1.190														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	321.66	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	1183	1129	1065	1049	1008	824	643	532	439	437	340	260	175	142
H ₂	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000	0.85000
H ₂ O	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000	0.15000
R = 0.20, PERCENT FUEL = 38.65, O/F = 1.587														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	324.94	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	1514	1450	1398	1354	1307	1079	852	709	588	585	458	379	242	198
H ₂	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000	0.80000
H ₂ O	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000	0.20000
R = 0.25, PERCENT FUEL = 33.51, O/F = 1.984														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	327.81	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	1817	1745	1686	1636	1567	1322	1057	867	741	737	561	462	310	256
H	0.00006	0.00003	0.00002	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.74955	0.74997	0.74998	0.74999	0.74999	0.75000	0.75000	0.75000	0.75000	0.75000	0.75000	0.75000	0.75000	0.75000
H ₂ O	0.24999	0.24999	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000	0.25000
R = 0.31, PERCENT FUEL = 29.57, O/F = 2.381														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	330.21	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	2094	2016	1952	1898	1847	1553	1257	1064	895	891	707	590	383	317
H	0.00039	0.00026	0.00018	0.00013	0.00009	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.69967	0.69978	0.69985	0.69989	0.69992	0.69999	0.70000	0.70000	0.70000	0.70000	0.70000	0.70000	0.70000	0.70000
H ₂ O	0.29992	0.29995	0.29998	0.29998	0.29998	0.30000	0.30000	0.30000	0.30000	0.30000	0.30000	0.30000	0.30000	0.30000
OH	0.00002	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
R = 0.35, PERCENT FUEL = 26.47, O/F = 2.778														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	332.36	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	2347	2266	2199	2140	2089	1771	1451	1238	1050	1045	838	702	460	382
H	0.00154	0.00111	0.00083	0.00063	0.00049	0.00007	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.64875	0.64910	0.64933	0.64949	0.64960	0.64994	0.65000	0.65000	0.65000	0.65000	0.65000	0.65000	0.65000	0.65000
H ₂ O	0.34956	0.34969	0.34978	0.34984	0.34988	0.34998	0.35000	0.35000	0.35000	0.35000	0.35000	0.35000	0.35000	0.35000
OH	0.00015	0.00009	0.00006	0.00004	0.00003	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
R = 0.40, PERCENT FUEL = 23.95, O/F = 3.175														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	334.53	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	2574	2492	2422	2365	2312	1978	1637	1408	1204	1199	970	818	542	452
H	0.00416	0.00320	0.00252	0.00203	0.00167	0.00034	0.00003	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.59881	0.59753	0.59805	0.59842	0.59870	0.59973	0.59998	0.60000	0.60000	0.60000	0.60000	0.60000	0.60000	0.60000
H ₂ O	0.39839	0.39882	0.39910	0.39930	0.39944	0.39991	0.39999	0.40000	0.40000	0.40000	0.40000	0.40000	0.40000	0.40000
OH	0.00054	0.00045	0.00033	0.00024	0.00019	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
R = 0.45, PERCENT FUEL = 21.87, O/F = 3.571														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	336.72	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	2773	2692	2624	2565	2517	2174	1817	1575	1357	1350	1104	927	629	526
H	0.00856	0.00695	0.00561	0.00483	0.00417	0.00112	0.00015	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
O	0.00002	0.00001	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.54383	0.54456	0.54591	0.54694	0.54694	0.54916	0.54989	0.54998	0.55000	0.55000	0.55000	0.55000	0.55000	0.55000
H ₂ O	0.44560	0.44559	0.44728	0.44779	0.44814	0.44959	0.44996	0.44999	0.45000	0.45000	0.45000	0.45000	0.45000	0.45000
O ₂	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
OH	0.00198	0.00149	0.00115	0.00091	0.00074	0.00013	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
R = 0.50, PERCENT FUEL = 20.12, O/F = 3.968														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	338.88	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	2944	2866	2800	2742	2699	2356	1990	1737	1507	1501	1238	1059	720	606
H	0.01447	0.01278	0.01057	0.00921	0.00825	0.00282	0.00053	0.00010	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000
O	0.00009	0.00006	0.00004	0.00003	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.49042	0.49180	0.49288	0.49376	0.49438	0.49801	0.49962	0.49992	0.49999	0.49999	0.50000	0.50000	0.50000	0.50000
H ₂ O	0.49024	0.49207	0.49342	0.49446	0.49510	0.49880	0.49990	0.49999	0.50000	0.50000	0.50000	0.50000	0.50000	0.50000
O ₂	0.00003	0.00002	0.00002	0.00001	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
OH	0.00475	0.00377	0.00307	0.00253	0.00218	0.00050	0.00005	0.00001	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
R = 0.60, PERCENT FUEL = 17.35, O/F = 4.762														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	342.61	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	3208	3137	3077	3025	2990	2669	2313	2050	1803	1796	1508	1306	916	778
H	0.02778	0.02508	0.02282	0.02094	0.01970	0.00988	0.00321	0.00110	0.00023	0.00022	0.00002	0.00000	0.00000	0.00000
O	0.00069	0.00054	0.00043	0.00035	0.00030	0.00006	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.38531	0.38701	0.38859	0.38998	0.39139	0.39582	0.39882	0.39962	0.39999	0.39999	0.39999	0.40000	0.40000	0.40000
H ₂ O	0.56931	0.57150	0.57350	0.57548	0.57610	0.58191	0.58796	0.58998	0.59000	0.59000	0.59000	0.59000	0.59000	0.59000
O ₂	0.00041	0.00037	0.00028	0.00021	0.00018	0.00004	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
OH	0.01629	0.01406	0.01233	0.01088	0.00998	0.00379	0.00131	0.00017	0.00002	0.00002	0.00000	0.00000	0.00000	0.00000
R = 0.70, PERCENT FUEL = 15.25, O/F = 5.556														
Pressure, lb/sq in. abs	600.00	500.00	428.57	375.00	345.24	150.00	60.00	30.00	15.00	14.70	6.00	3.00	0.60	0.30
Temperature, °K	3381	3320	3263	3217	3180	2803	2364	2057	1808	1801	1575	1356	1125	966
H	0.03771	0.03524	0.03316	0.03136	0.03028	0.01959	0.00964	0.00443	0.00158	0.00151	0.00025	0.00004	0.00000	0.00000
O	0.00069	0.00054	0.00043	0.00035	0.00030	0.00006	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
H ₂	0.29582	0.29730	0.29849	0.29939	0.29999	0.30584	0.31191	0.31799	0.32399	0.32399	0.32399	0.32399	0.32399	0.32399
H ₂ O	0.42760	0.43436	0.43959	0.44449	0.44899	0.46471	0.47154	0.47800	0.48399	0.48399	0.48399	0.48399	0.48399	0.48399
O ₂	0.00289	0.00199	0.00175	0.00155	0.00143	0.00054	0.00011	0.00002	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000

TABLE IV. - Concluded. EQUILIBRIUM COMPOSITION OF PRODUCTS OF REACTION AT ASSIGNED PRESSURES FOR LIQUID HYDROGEN AND LIQUID OXYGEN

[Isentropic expansion from chamber conditions; compositions are given in mole fractions. Equivalence ratio, R; oxidant-fuel ratio, O/F.]

(d) Concluded. Combustion-chamber pressure, 600 pounds per square inch absolute

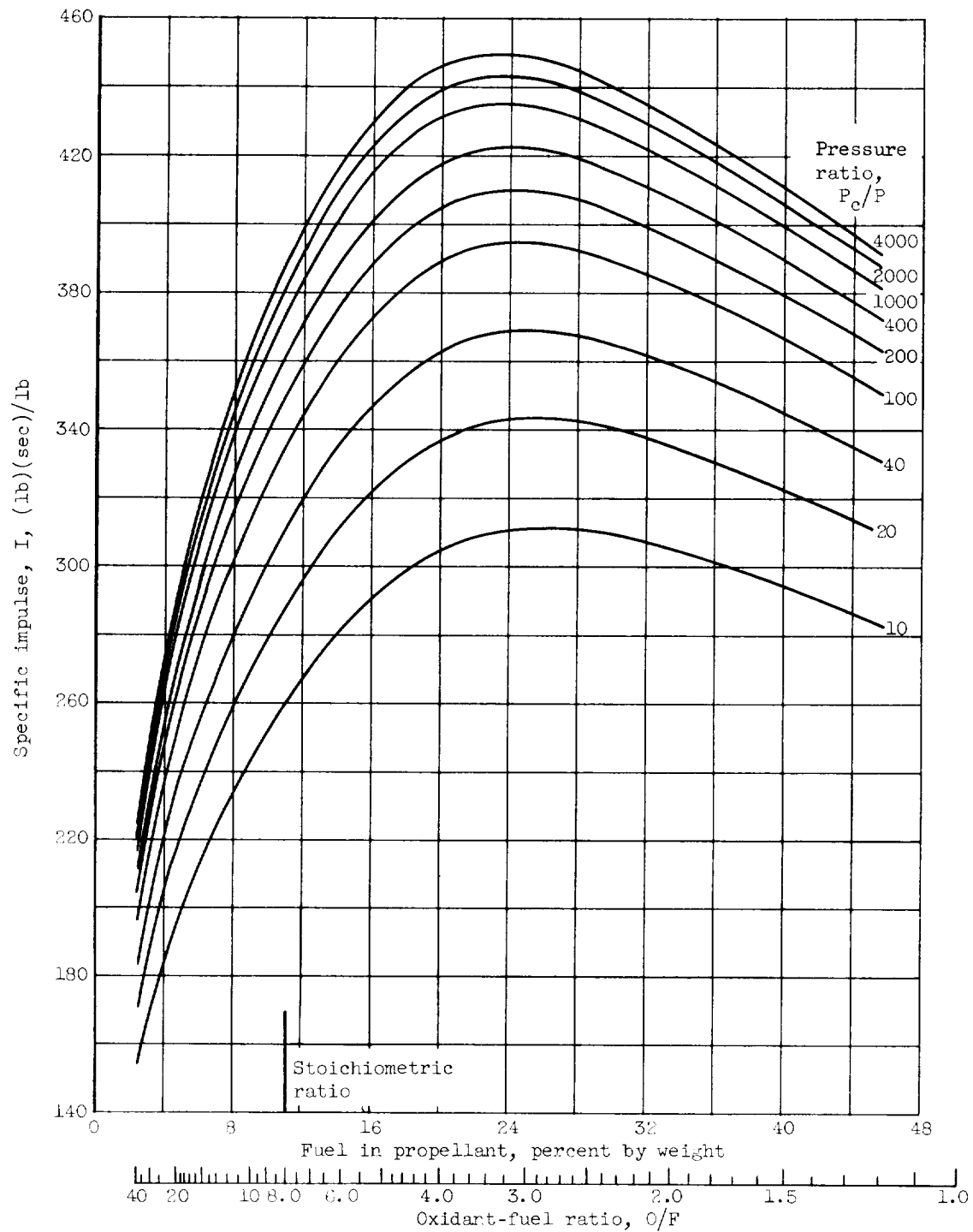
Table with multiple sections for different R values (0.80, 0.90, 1.00, 1.50, 2.00, 3.00, 4.00, 5.00). Each section includes a header row for Pressure and Temperature, and a grid of mole fractions for species H, O, H2, H2O, O2, and OH at various conditions.

TABLE V. - SUMMARY OF COMBUSTION PARAMETERS, CHARACTERISTIC VELOCITY, AND PERFORMANCE FOR EXPANSION TO SEA LEVEL FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

Equivalence ratio, R_1 $2(O)/H$	Fuel, percent by weight	Oxidant-fuel ratio, O/F	Combustion temperature, T_c , °C	Exit temperature, T_e , °K	Characteristic velocity, c^* , ft/sec	Characteristic velocity exponent, n_{c^*}	Entropy, s , cal/(g)(°K)	Area ratio, ϵ	Coefficient of thrust, C_F	Specific impulse, I_s , (lb)(sec)/lb
CHAMBER PRESSURE, 60 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION										
0.150	45.65	1.190	1183	819	7247	0.0000	4.3807	1.244	1.038	231.7
.200	38.65	1.587	1514	1073	7607	.0000	4.5172	1.256	1.035	244.7
.250	33.51	1.984	1816	1316	7814	.0000	7.8147	1.268	1.033	250.8
.300	29.57	2.381	2093	1546	7930	.0000	7.2390	1.278	1.031	254.1
.350	26.47	2.778	2329	1764	7988	.0001	6.7611	1.289	1.029	255.4
.400	23.95	3.175	2531	1970	8001	.0009	6.3590	1.302	1.027	255.3
.450	21.87	3.571	2696	2159	7975	.0025	6.0167	1.316	1.025	254.0
.500	20.12	3.968	2828	2321	7912	.0045	5.7222	1.331	1.024	251.8
.600	17.35	4.762	3015	2588	7729	.0080	5.2415	1.354	1.023	245.7
.700	15.25	5.556	3128	2756	7508	.0105	4.8659	1.369	1.022	238.6
.800	13.60	6.349	3188	2848	7277	.0119	4.5644	1.376	1.022	231.2
.900	12.28	7.143	3213	2888	7034	.0125	4.3159	1.379	1.022	224.1
1.000	11.19	7.937	3217	2886	6846	.0126	4.1101	1.380	1.022	217.5
1.500	7.749	11.905	3116	2711	6081	.0169	3.4371	1.377	1.022	192.6
2.000	5.927	15.873	2786	2297	5250	.0087	3.0853	1.368	1.022	176.4
3.000	4.031	23.810	2025	1207	4866	.0040	2.8610	1.339	1.023	154.8
4.000	3.054	31.746	2347	1851	4366	.0009	2.4399	1.311	1.026	139.2
5.000	2.458	39.683	2062	1571	3972	.0001	2.2959	1.295	1.029	127.0
CHAMBER PRESSURE, 150 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION										
0.150	45.65	1.190	1183	819	7247	0.0000	8.7684	1.497	1.261	284.0
.200	38.65	1.587	1514	1073	7607	.0000	8.1681	2.033	1.261	298.2
.250	33.51	1.984	1816	1316	7814	.0000	7.5120	2.073	1.262	306.6
.300	29.57	2.381	2093	1546	7929	.0000	6.9718	2.111	1.264	311.5
.350	26.47	2.778	2329	1764	7988	.0000	6.5215	2.147	1.265	314.0
.400	23.95	3.175	2531	1970	8006	.0005	6.1415	2.182	1.266	315.0
.450	21.87	3.571	2733	2159	7988	.0016	5.8170	2.221	1.267	314.7
.500	20.12	3.968	2881	2321	7940	.0033	5.5371	2.264	1.270	313.3
.600	17.35	4.762	3097	2588	7782	.0068	5.0787	2.352	1.275	308.4
.700	15.25	5.556	3231	2844	7577	.0093	4.7193	2.425	1.280	301.4
.800	13.60	6.349	3304	2899	7355	.0113	4.4299	2.472	1.282	293.2
.900	12.28	7.143	3336	2770	7134	.0121	4.1919	2.493	1.284	284.6
1.000	11.19	7.937	3341	2785	6925	.0122	3.9926	2.498	1.284	276.4
1.500	7.749	11.905	3219	2621	6120	.0163	3.3416	2.474	1.283	246.0
2.000	5.927	15.873	3045	2382	5592	.0079	2.9807	2.427	1.280	222.4
3.000	4.031	23.810	2895	1907	4882	.0032	2.5869	2.301	1.272	193.0
4.000	3.054	31.746	2363	1549	4369	.0007	2.3706	2.215	1.267	172.1
5.000	2.458	39.683	2066	1298	3972	.0000	2.2298	2.171	1.266	156.3
CHAMBER PRESSURE, 300 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION										
0.150	45.65	1.190	1183	819	7247	0.0000	8.0565	3.020	1.379	310.6
.200	38.65	1.587	1514	1073	7607	.0000	7.4040	3.088	1.382	326.7
.250	33.51	1.984	1817	1317	7813	.0000	7.2831	3.168	1.386	336.5
.300	29.57	2.381	2093	1549	7929	.0000	6.7696	3.248	1.390	342.5
.350	26.47	2.778	2344	1764	7988	.0000	6.3404	3.325	1.393	345.9
.400	23.95	3.175	2565	1970	8008	.0003	5.9772	3.399	1.397	347.6
.450	21.87	3.571	2755	2189	7988	.0012	5.6888	3.474	1.401	348.1
.500	20.12	3.968	2915	2321	7956	.0025	5.3978	3.525	1.405	347.5
.600	17.35	4.762	3125	2587	7816	.0058	4.9564	3.728	1.416	343.9
.700	15.25	5.556	3307	2828	7625	.0087	4.6094	3.900	1.426	337.9
.800	13.60	6.349	3393	2844	7411	.0107	4.3293	4.042	1.433	330.1
.900	12.28	7.143	3430	2801	7193	.0117	4.0983	4.121	1.437	321.2
1.000	11.19	7.937	3437	2807	6983	.0118	3.9046	4.140	1.438	312.0
1.500	7.749	11.905	3297	2472	6183	.0097	3.2701	4.028	1.434	274.6
2.000	5.927	15.873	3103	2181	5621	.0072	2.9171	3.918	1.426	249.2
3.000	4.031	23.810	2723	1876	4892	.0027	2.5510	3.634	1.410	214.4
4.000	3.054	31.746	2372	1543	4371	.0005	2.3183	3.474	1.400	190.2
5.000	2.458	39.683	2069	1217	3972	.0000	2.1794	3.368	1.396	172.4
CHAMBER PRESSURE, 600 POUNDS PER SQUARE INCH ABSOLUTE, EQUILIBRIUM COMPOSITION										
0.150	45.65	1.190	1183	819	7247	0.0000	6.3446	4.862	1.469	338.9
.200	38.65	1.587	1514	1073	7607	.0000	7.6399	4.862	1.474	348.6
.250	33.51	1.984	1817	1317	7813	.0000	7.0541	4.945	1.481	359.6
.300	29.57	2.381	2093	1549	7929	.0000	6.5675	5.106	1.488	366.6
.350	26.47	2.778	2347	1764	7988	.0000	6.1594	5.260	1.494	370.9
.400	23.95	3.175	2574	1977	8010	.0002	5.8131	5.409	1.500	373.4
.450	21.87	3.571	2773	2190	8001	.0009	5.5100	5.554	1.506	374.5
.500	20.12	3.968	2944	2321	7968	.0019	5.2683	5.701	1.512	374.5
.600	17.35	4.762	3208	2587	7844	.0046	4.8347	6.013	1.527	372.3
.700	15.25	5.556	3381	2801	7669	.0077	4.5002	6.350	1.534	367.6
.800	13.60	6.349	3461	2845	7485	.0100	4.2294	6.687	1.535	360.6
.900	12.28	7.143	3460	2843	7290	.0111	4.0096	6.997	1.535	352.7
1.000	11.19	7.937	3434	2812	7093	.0114	3.8175	7.322	1.536	342.0
1.500	7.749	11.905	3374	2603	6203	.0091	3.1996	6.780	1.537	300.2
2.000	5.927	15.873	3128	2327	5648	.0065	2.8535	6.416	1.544	271.1
3.000	4.031	23.810	2747	1884	4900	.0023	2.4722	5.862	1.520	231.4
4.000	3.054	31.746	2361	1527	4372	.0004	2.2627	5.272	1.509	204.7
5.000	2.458	39.683	2072	1227	3972	.0000	2.1270	5.405	1.498	183.1

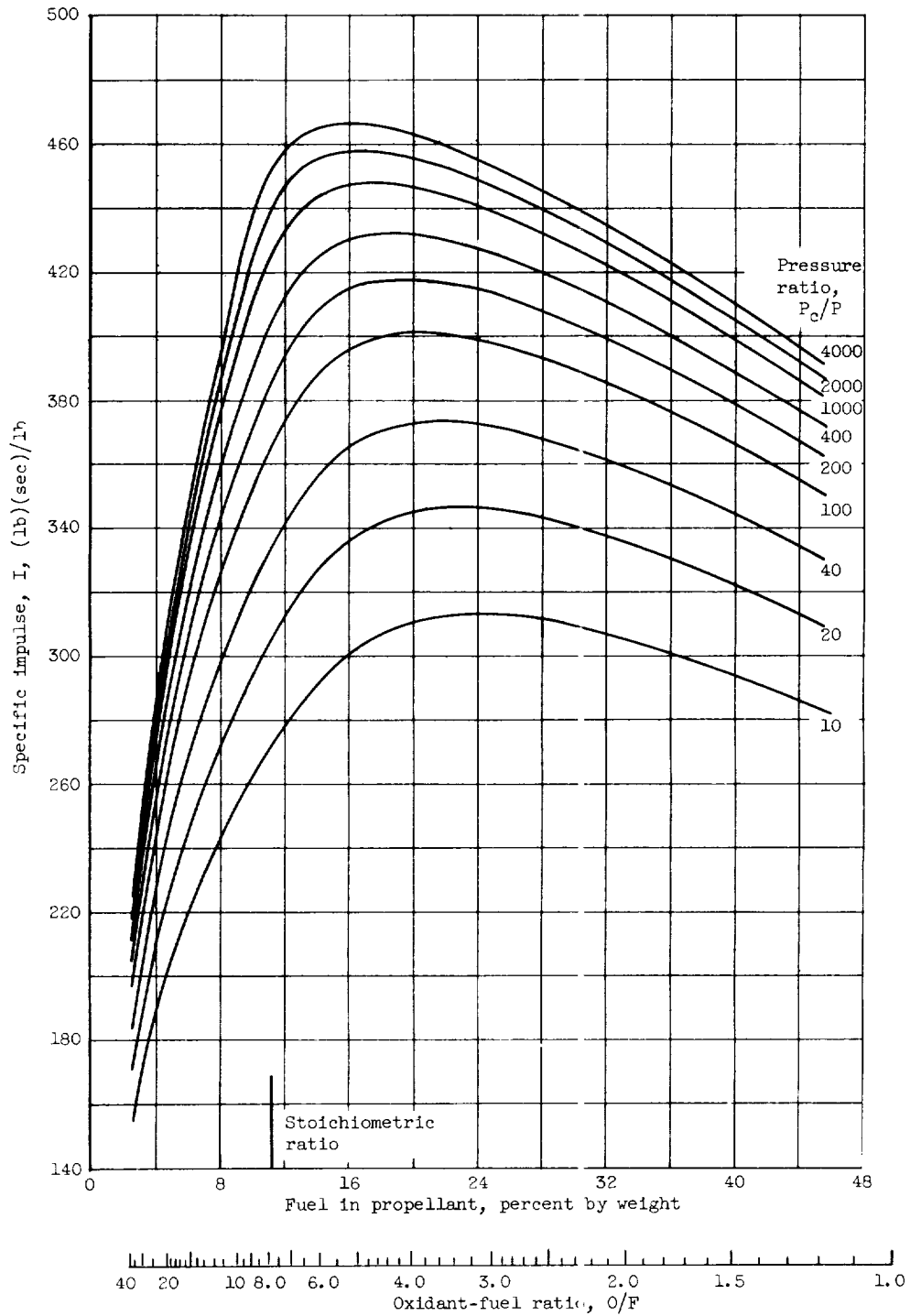
TABLE V. - Concluded. SUMMARY OF COMBUSTION PARAMETERS, CHARACTERISTIC VELOCITY, AND PERFORMANCE FOR EXPANSION TO SEA LEVEL FOR LIQUID HYDROGEN WITH LIQUID OXYGEN

Equivalence ratio, $R = 2(O)/H$	Fuel, percent by weight	Oxidant-fuel weight ratio, O/F	Combustion temperature, T_c, O_K	Exit temperature, T_e, O_K	Characteristic velocity, c^* , ft/sec	Entropy, s , cal/(g)(°K)	Area ratio, ϵ	Coefficient of thrust, C_F	Specific impulse, I_{sp} , (lb)(sec)/lb
CHAMBER PRESSURE, 60 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	819	7247	9.3607	1.244	1.038	253.7
.200	38.65	1.587	1514	1073	7607	8.5172	1.256	1.035	244.7
.250	33.51	1.984	1816	1215	7811	7.8147	1.267	1.033	239.8
.300	29.57	2.381	2089	1340	7916	7.2590	1.278	1.032	235.8
.350	26.47	2.778	2329	1441	7948	6.7811	1.286	1.030	231.6
.400	23.95	3.175	2531	1512	7922	6.3590	1.292	1.030	228.5
.450	21.87	3.571	2696	2053	7856	6.0167	1.297	1.029	225.3
.500	20.12	3.968	2828	2166	7763	5.7122	1.301	1.029	218.2
.600	17.35	4.762	3015	2330	7542	5.2415	1.307	1.028	211.0
.700	15.25	5.556	3128	2429	7304	4.8859	1.310	1.028	203.3
.800	13.60	6.349	3188	2484	7070	4.5644	1.312	1.028	225.8
.900	12.28	7.143	3213	2506	6820	4.2839	1.313	1.027	218.8
1.000	11.19	7.937	3217	2514	6648	4.1101	1.313	1.027	212.3
1.500	7.749	11.905	3116	2433	5891	3.4471	1.313	1.028	188.1
2.000	5.927	15.873	2966	2308	5401	3.0035	1.311	1.028	172.5
3.000	4.031	23.810	2655	2046	4786	2.6610	1.305	1.028	152.3
4.000	3.054	31.746	2347	1789	4316	2.4239	1.298	1.029	138.1
5.000	2.458	39.683	2062	1554	3954	2.2465	1.292	1.030	126.6
CHAMBER PRESSURE, 150 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	639	7247	8.9684	1.997	1.261	284.0
.200	38.65	1.587	1514	847	7607	8.1681	2.033	1.261	298.2
.250	33.51	1.984	1816	1052	7812	7.5120	2.072	1.263	306.5
.300	29.57	2.381	2089	1248	7921	6.9718	2.110	1.264	311.2
.350	26.47	2.778	2329	1430	7961	6.5115	2.142	1.265	313.1
.400	23.95	3.175	2531	1592	7920	6.1115	2.168	1.267	313.0
.450	21.87	3.571	2696	1733	7899	5.8170	2.189	1.268	311.2
.500	20.12	3.968	2828	1846	7821	5.5511	2.205	1.268	308.3
.600	17.35	4.762	3091	2019	7621	5.0737	2.228	1.269	300.7
.700	15.25	5.556	3231	2126	7395	4.7193	2.242	1.270	291.9
.800	13.60	6.349	3304	2190	7166	4.4499	2.251	1.271	283.0
.900	12.28	7.143	3336	2219	6947	4.1819	2.250	1.271	274.4
1.000	11.19	7.937	3341	2226	6743	3.9526	2.258	1.271	266.3
1.500	7.749	11.905	3219	2140	5965	3.3416	2.255	1.271	235.6
2.000	5.927	15.873	3045	2009	5458	2.9837	2.244	1.270	215.5
3.000	4.031	23.810	2695	1745	4796	2.5859	2.219	1.269	189.2
4.000	3.054	31.746	2363	1498	4329	2.3736	2.192	1.268	170.6
5.000	2.458	39.683	2066	1284	3958	2.2296	2.166	1.267	155.8
CHAMBER PRESSURE, 300 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	529	7247	8.6555	3.020	1.379	310.6
.200	38.65	1.587	1514	702	7607	7.9040	3.098	1.382	326.7
.250	33.51	1.984	1817	882	7812	7.2831	3.167	1.386	336.5
.300	29.57	2.381	2093	1057	7923	6.7646	3.247	1.390	342.2
.350	26.47	2.778	2344	1223	7969	6.3434	3.319	1.394	345.1
.400	23.95	3.175	2565	1376	7966	5.9772	3.380	1.397	345.8
.450	21.87	3.571	2755	1511	7926	5.6634	3.431	1.399	344.7
.500	20.12	3.968	2915	1627	7858	5.3976	3.471	1.401	342.3
.600	17.35	4.762	3122	1802	7675	4.9534	3.530	1.404	335.0
.700	15.25	5.556	3307	1922	7461	4.6074	3.587	1.406	326.1
.800	13.60	6.349	3393	1990	7237	4.3273	3.630	1.408	318.6
.900	12.28	7.143	3430	2023	7019	4.0933	3.662	1.408	307.2
1.000	11.19	7.937	3437	2031	6813	3.9046	3.697	1.409	298.3
1.500	7.749	11.905	3297	1940	6019	3.2731	3.579	1.408	263.4
2.000	5.927	15.873	3103	1804	5496	2.9171	3.569	1.406	240.4
3.000	4.031	23.810	2723	1540	4816	2.5310	3.505	1.403	210.0
4.000	3.054	31.746	2372	1304	4337	2.3113	3.439	1.400	188.7
5.000	2.458	39.683	2069	1107	3960	2.1774	3.380	1.397	171.9
CHAMBER PRESSURE, 600 POUNDS PER SQUARE INCH ABS., FROZEN COMPOSITION									
0.150	45.65	1.190	1183	437	7247	8.3446	4.682	1.469	330.9
.200	38.65	1.587	1514	585	7607	7.6319	4.802	1.474	348.6
.250	33.51	1.984	1817	736	7812	7.0511	4.949	1.481	359.6
.300	29.57	2.381	2093	889	7924	6.5055	5.104	1.488	366.4
.350	26.47	2.778	2347	1037	7974	6.0544	5.252	1.494	370.3
.400	23.95	3.175	2574	1181	7976	5.6831	5.384	1.499	371.6
.450	21.87	3.571	2773	1310	7947	5.3510	5.497	1.504	371.5
.500	20.12	3.968	2944	1424	7890	5.0532	5.591	1.508	369.7
.600	17.35	4.762	3205	1607	7725	4.6837	5.730	1.513	363.3
.700	15.25	5.556	3381	1721	7522	4.3502	5.821	1.517	354.6
.800	13.60	6.349	3461	1807	7306	4.0274	5.876	1.519	344.9
.900	12.28	7.143	3525	1844	7089	3.7006	5.906	1.520	335.0
1.000	11.19	7.937	3536	1851	6882	3.4817	5.919	1.521	325.3
1.500	7.749	11.905	3374	1736	6071	3.1910	5.887	1.519	285.7
2.000	5.927	15.873	3153	1616	5556	2.8937	5.816	1.517	261.0
3.000	4.031	23.810	2747	1355	4834	2.4872	5.667	1.510	226.9
4.000	3.054	31.746	2391	1127	4343	2.2809	5.621	1.509	203.1
5.000	2.458	39.683	2072	947	3962	2.1270	5.593	1.499	184.6



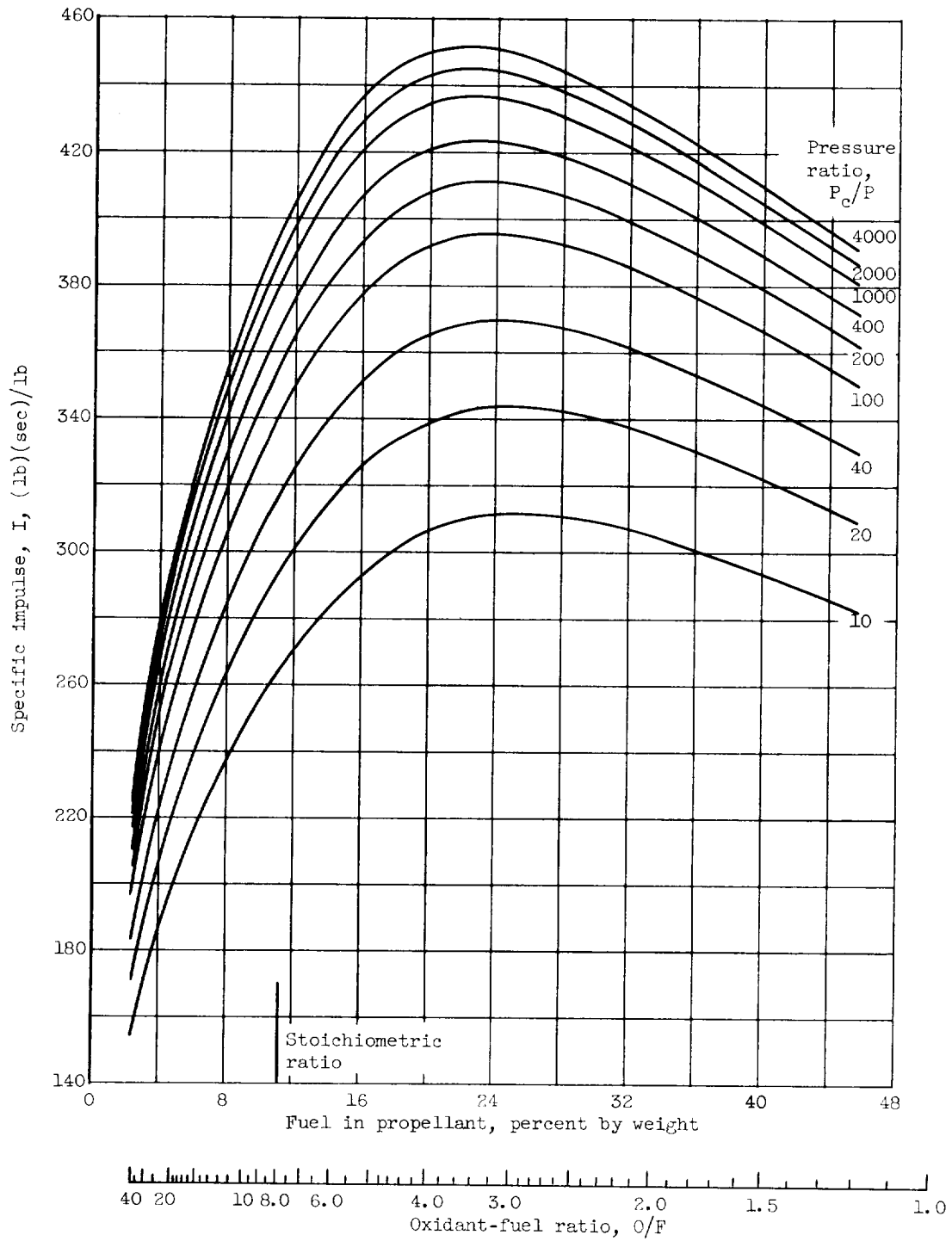
(a) Chamber pressure, 60 pounds per square inch absolute;
frozen composition during expansion.

Figure 1. - Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



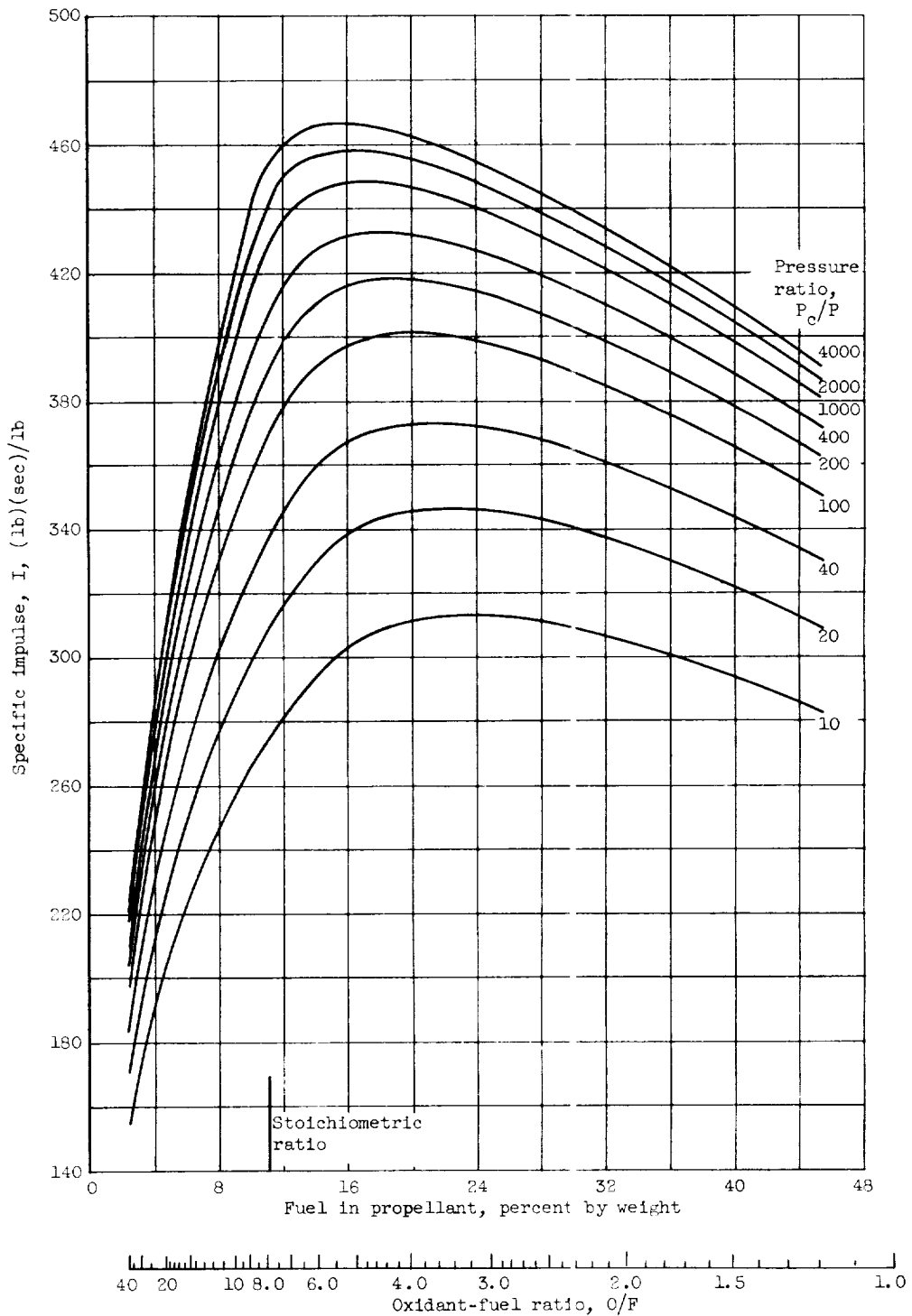
(b) Chamber pressure, 60 pounds per square inch absolute; equilibrium composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



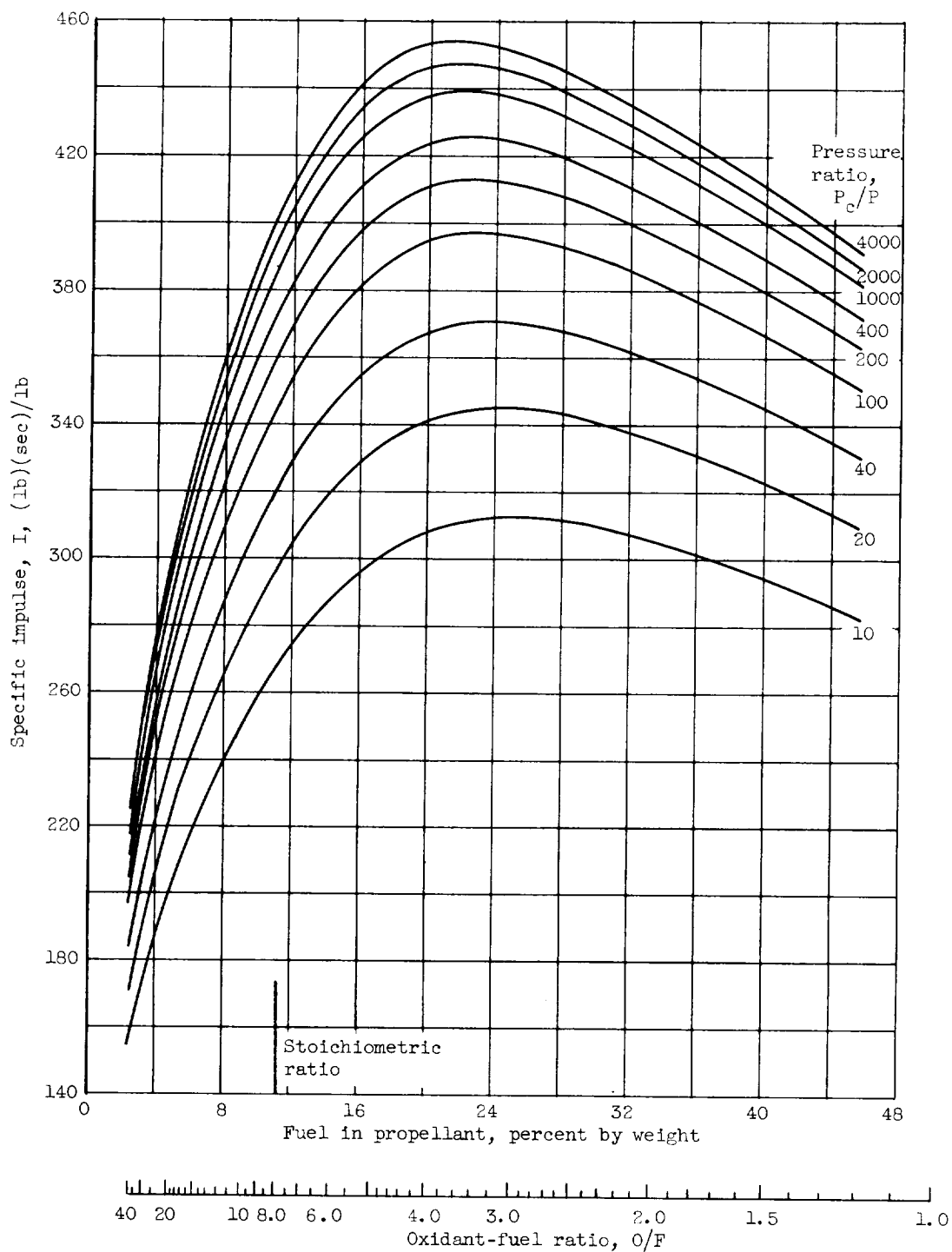
(c) Chamber pressure, 150 pounds per square inch absolute;
frozen composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



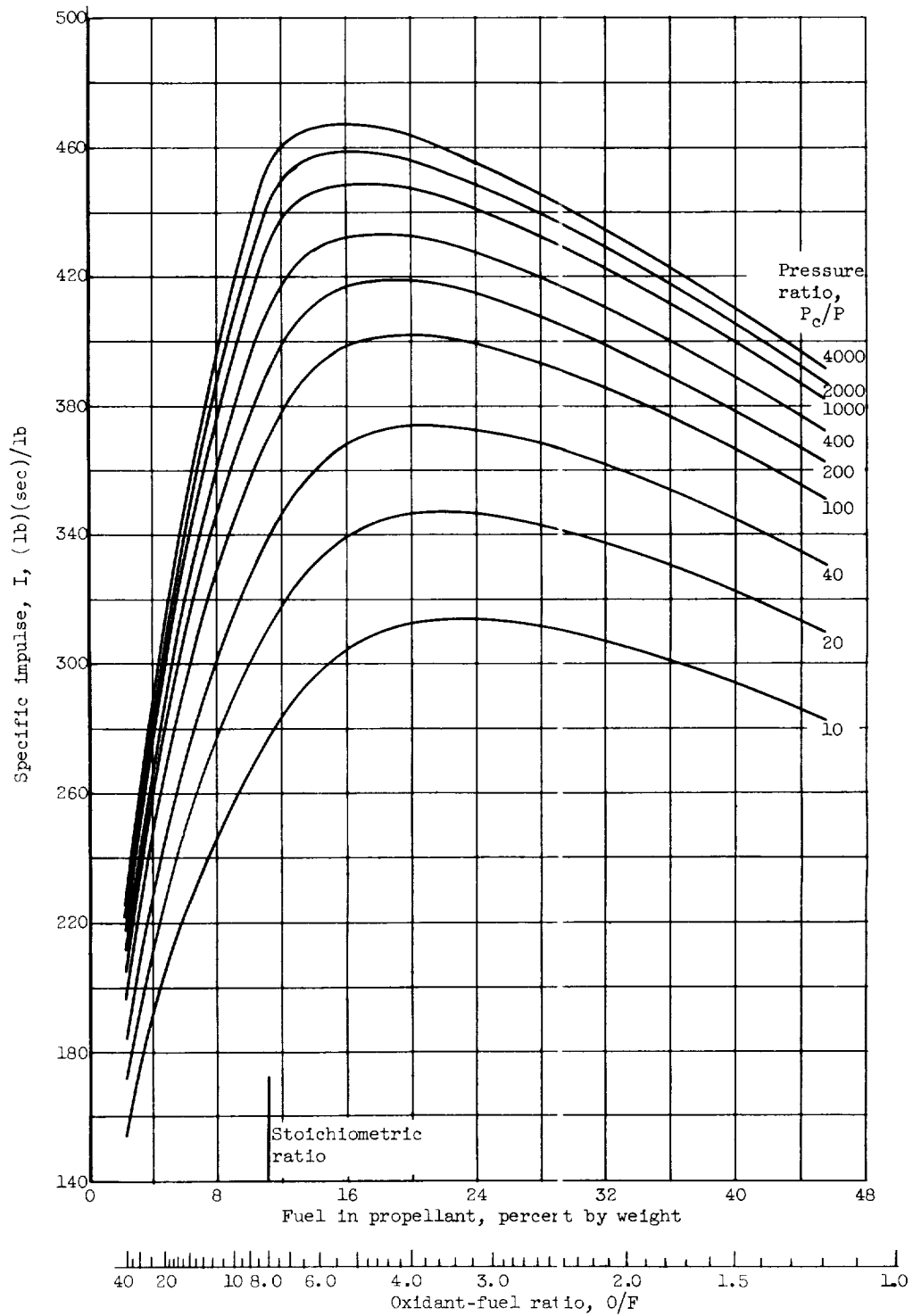
(d) Chamber pressure, 150 pounds per square inch absolute; equilibrium composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



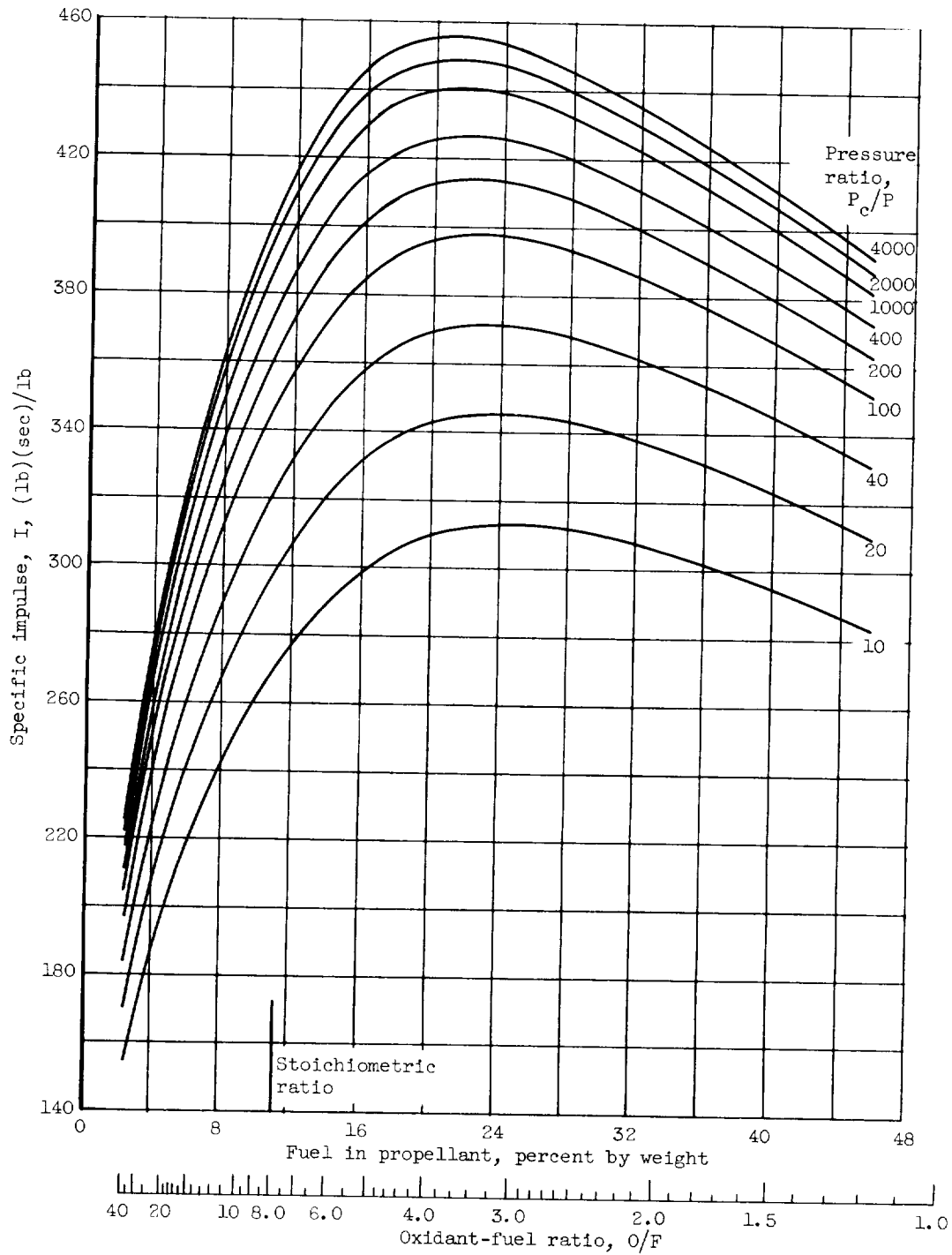
(e) Chamber pressure, 300 pounds per square inch absolute;
frozen composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



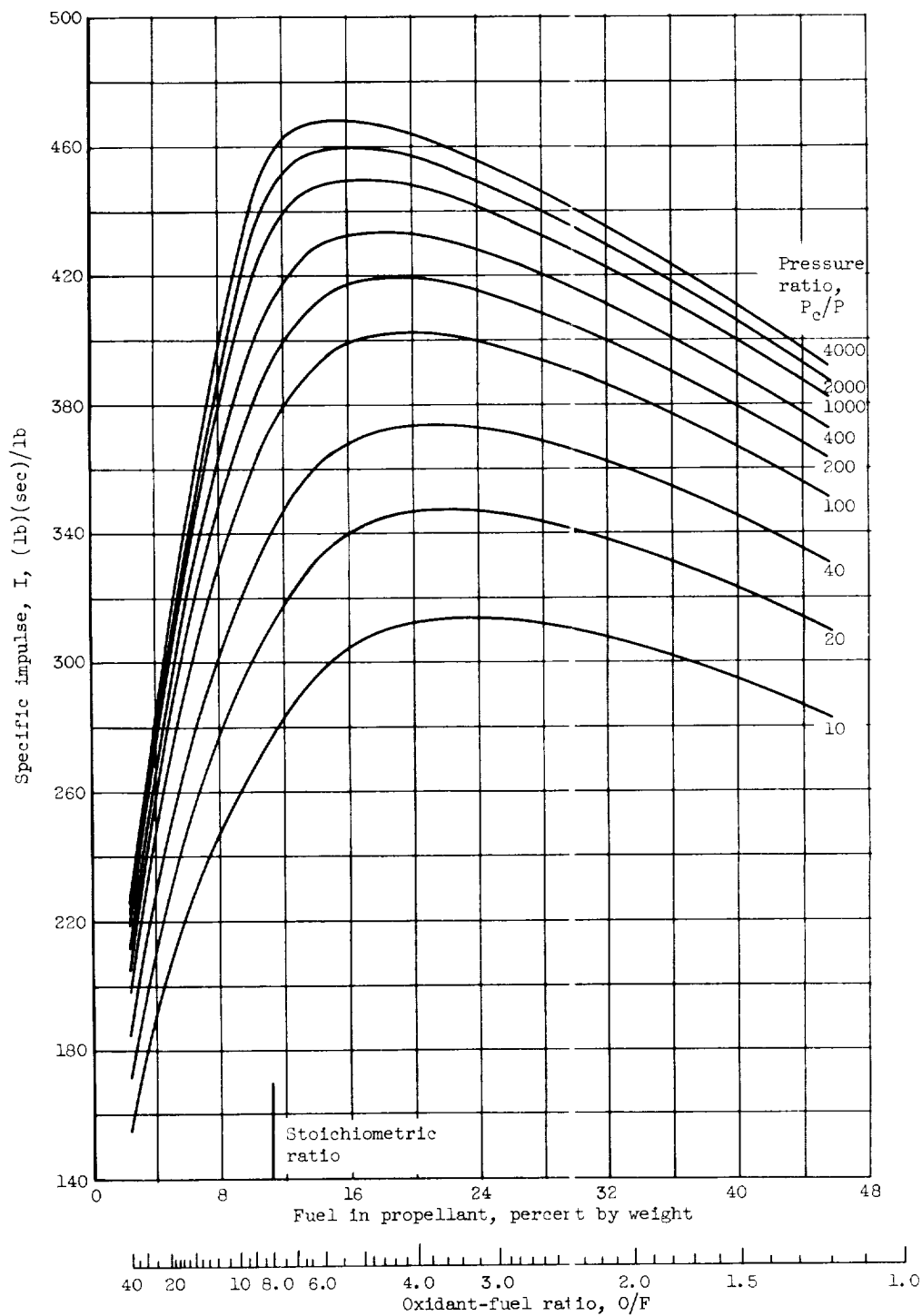
(f) Chamber pressure, 300 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



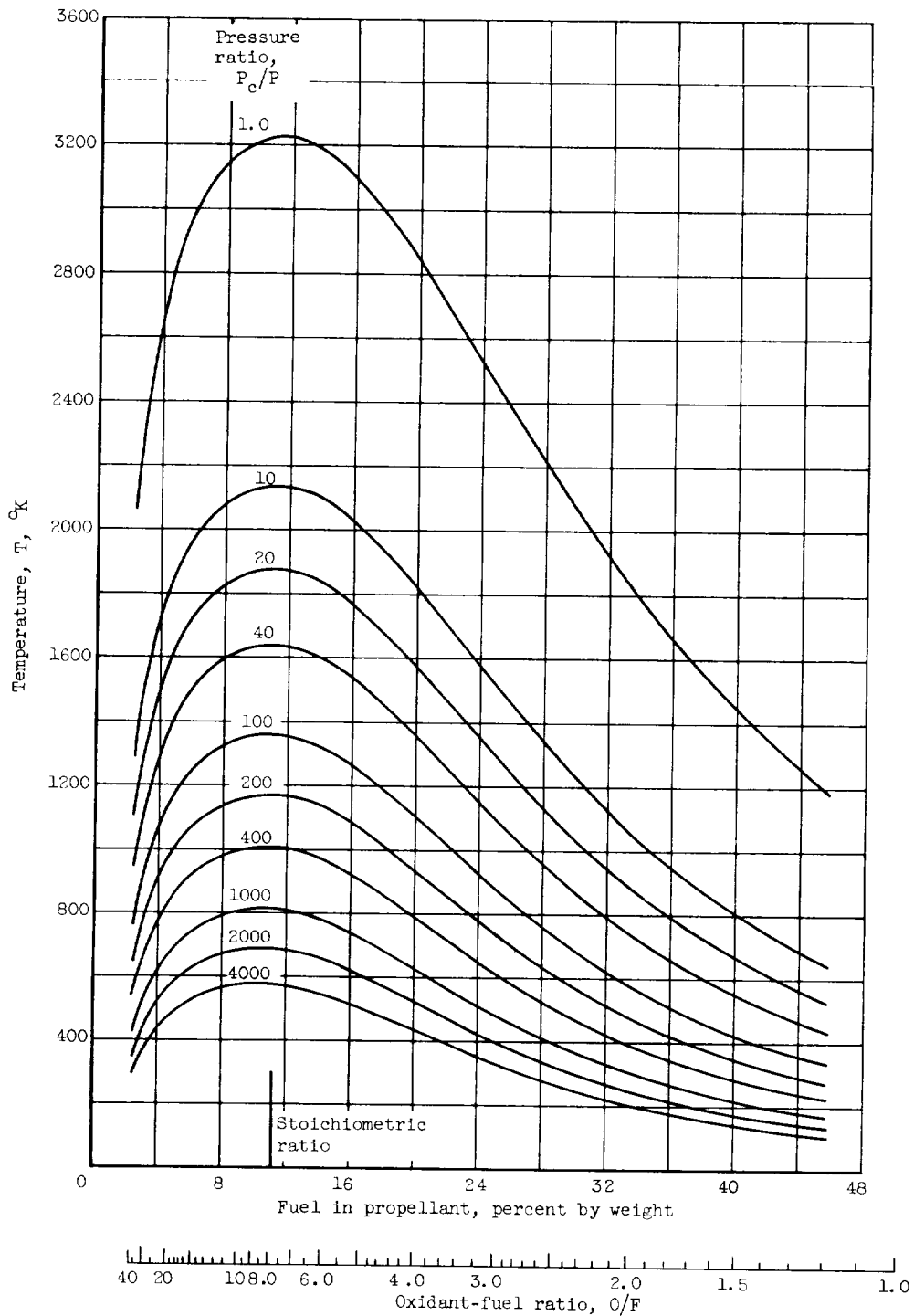
(g) Chamber pressure, 600 pounds per square inch absolute;
frozen composition during expansion.

Figure 1. - Continued. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



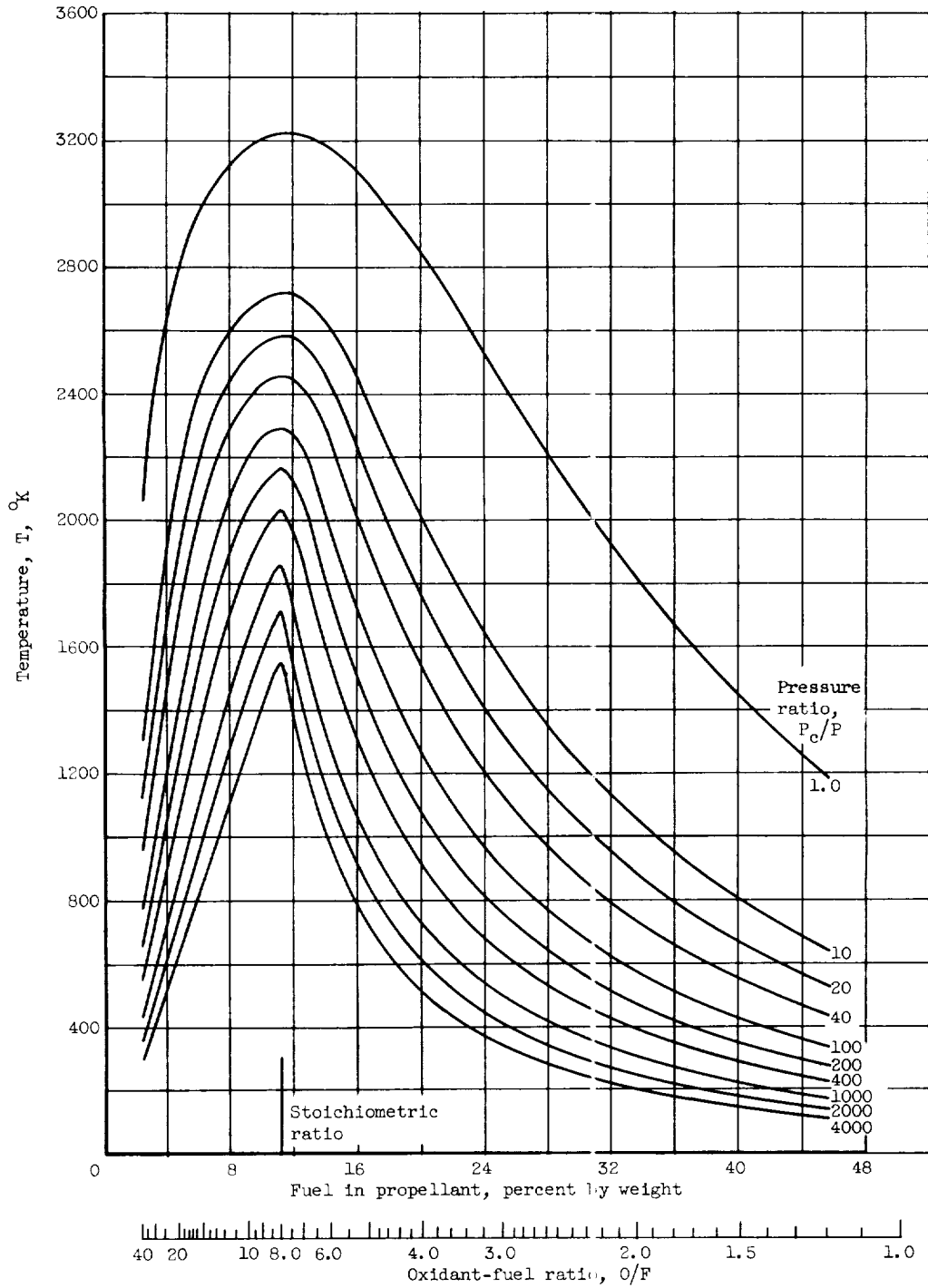
(h) Chamber pressure, 600 pounds per square inch absolute; equilibrium composition during expansion.

Figure 1. - Concluded. Theoretical specific impulse of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



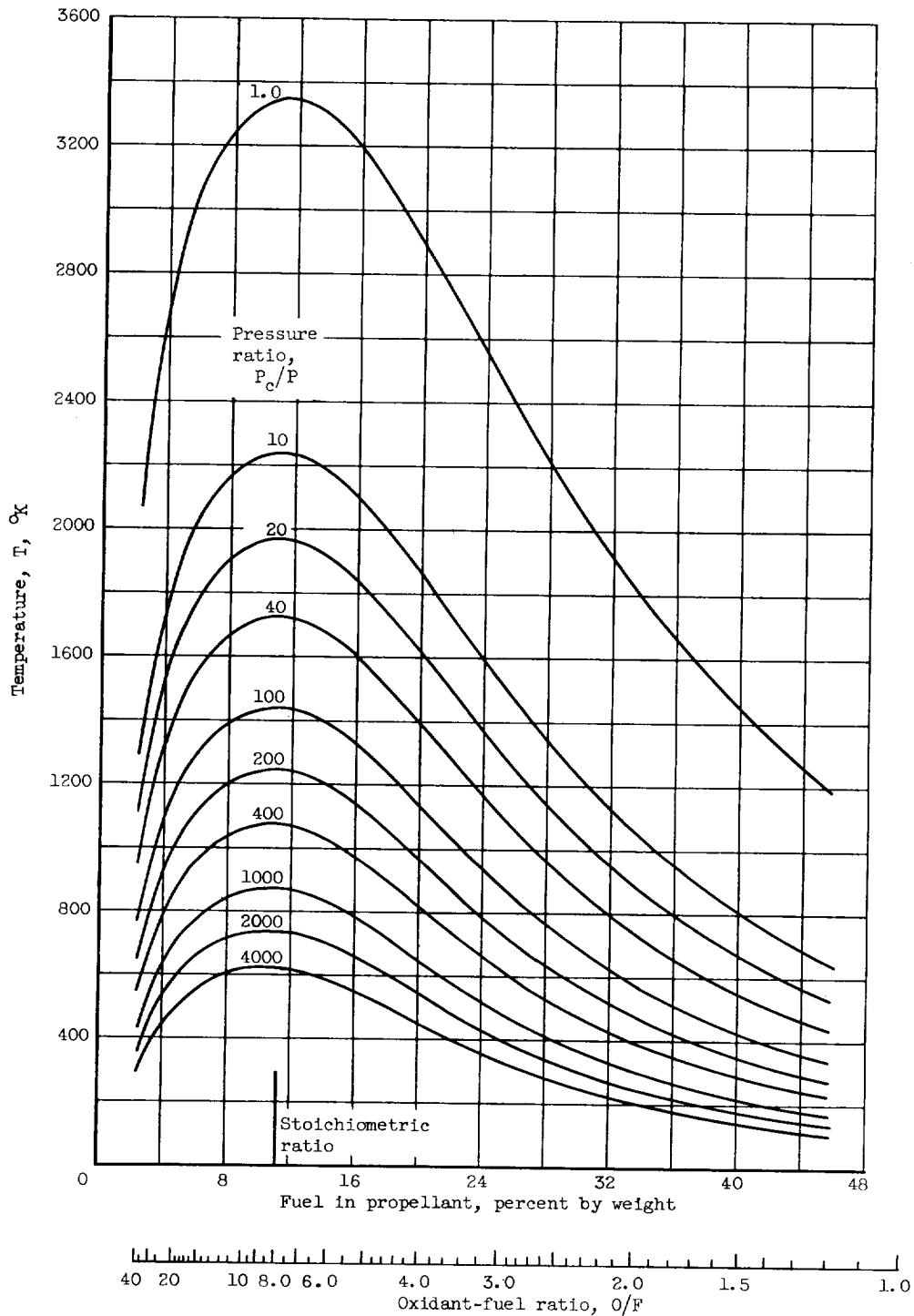
(a) Chamber pressure, 60 pounds per square inch absolute; frozen composition during expansion.

Figure 2. - Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



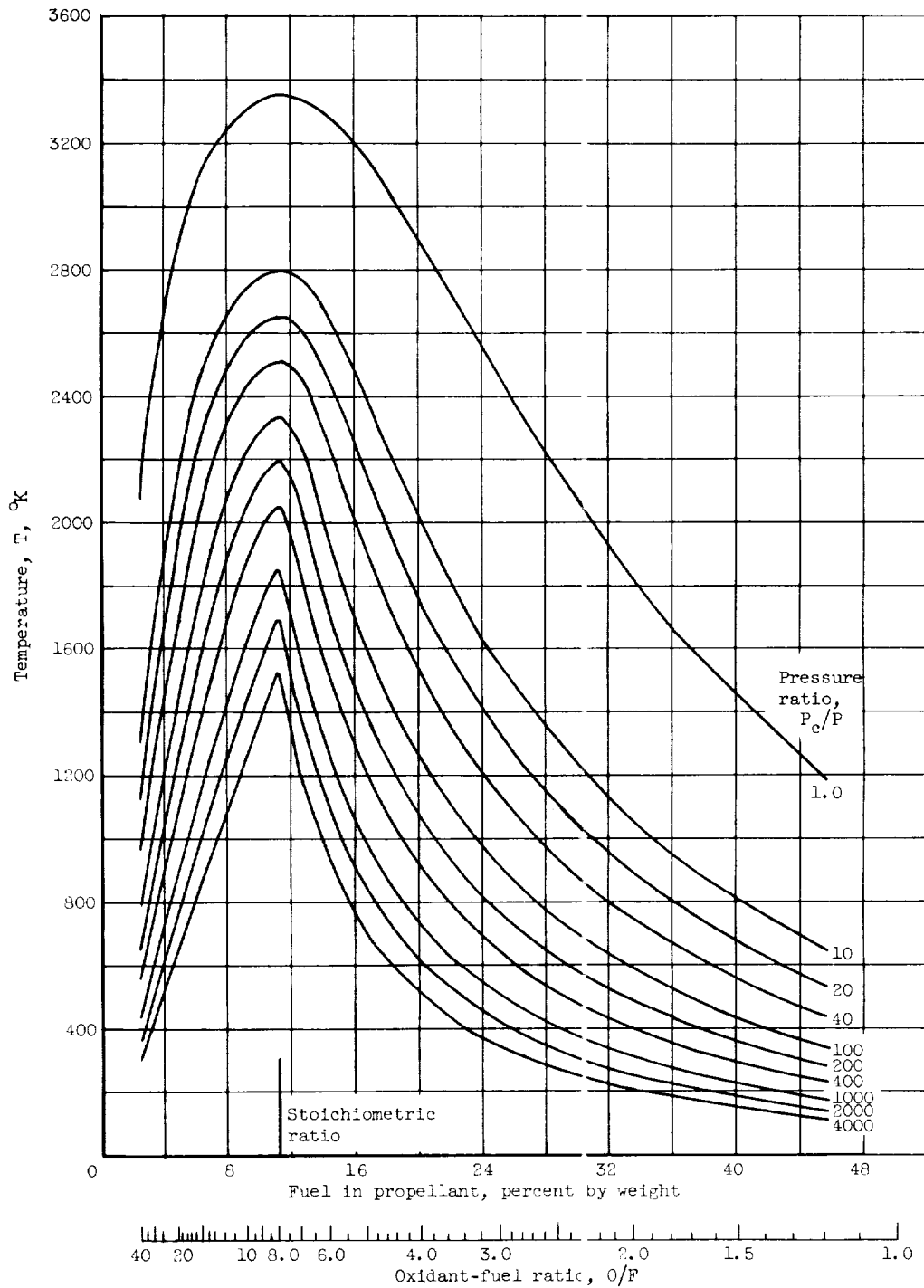
(b) Chamber pressure, 60 pounds per square inch absolute; equilibrium composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



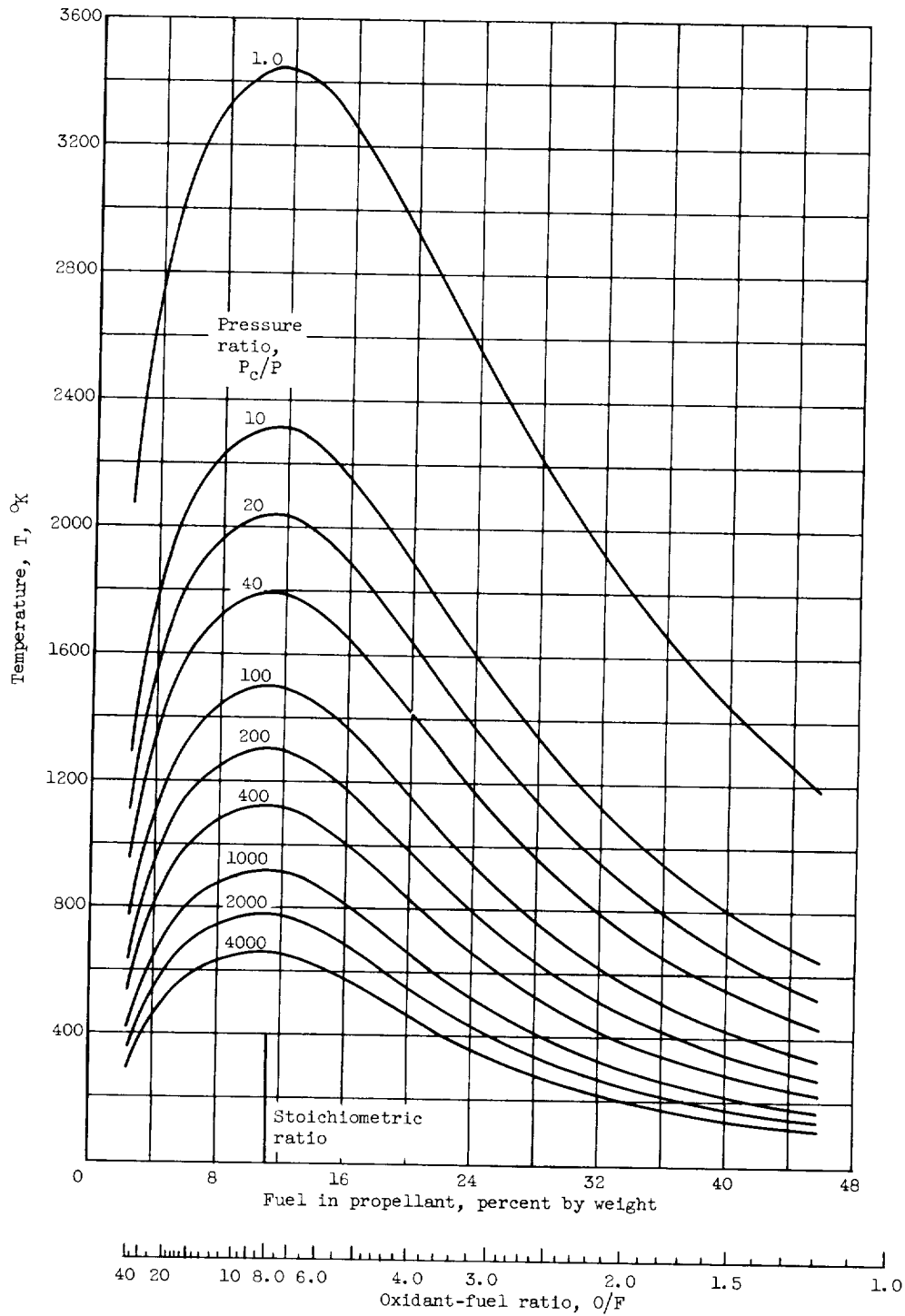
(c) Chamber pressure, 150 pounds per square inch absolute;
frozen composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



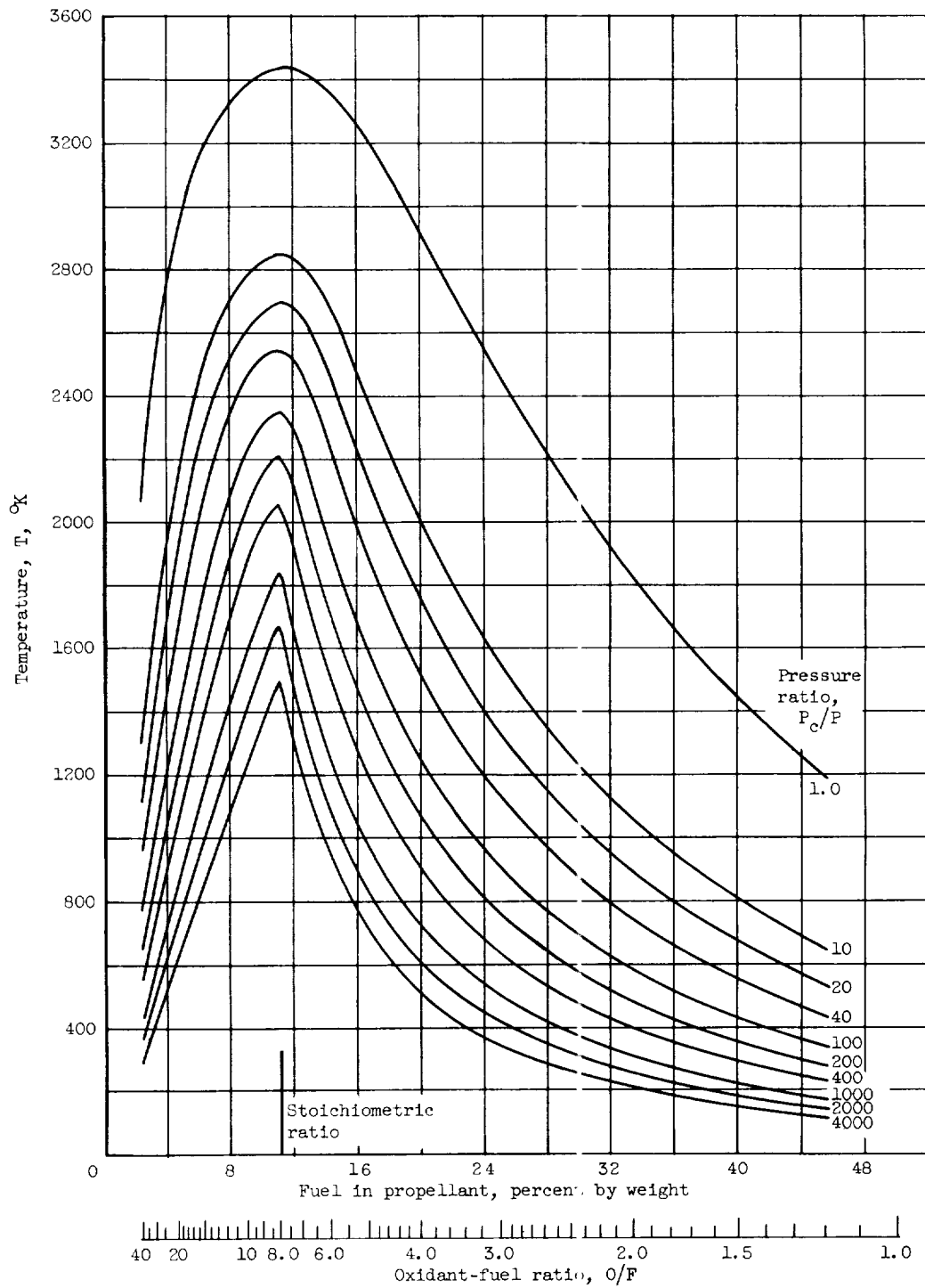
(d) Chamber pressure, 150 pounds per square inch absolute; equilibrium composition during expansion.

Figure 2. - Continued. Theoretical combustor chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



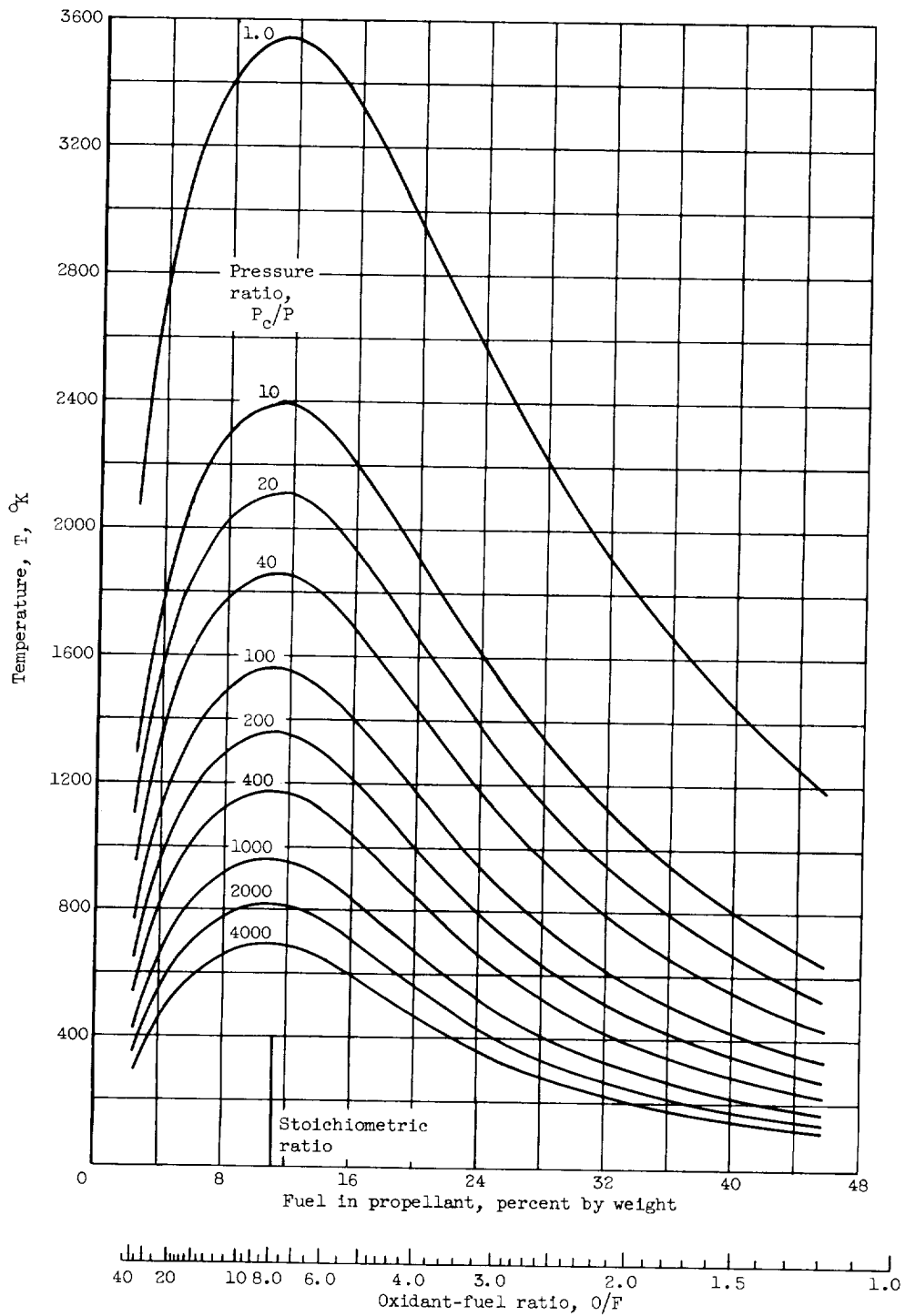
(e) Chamber pressure, 300 pounds per square inch absolute;
frozen composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



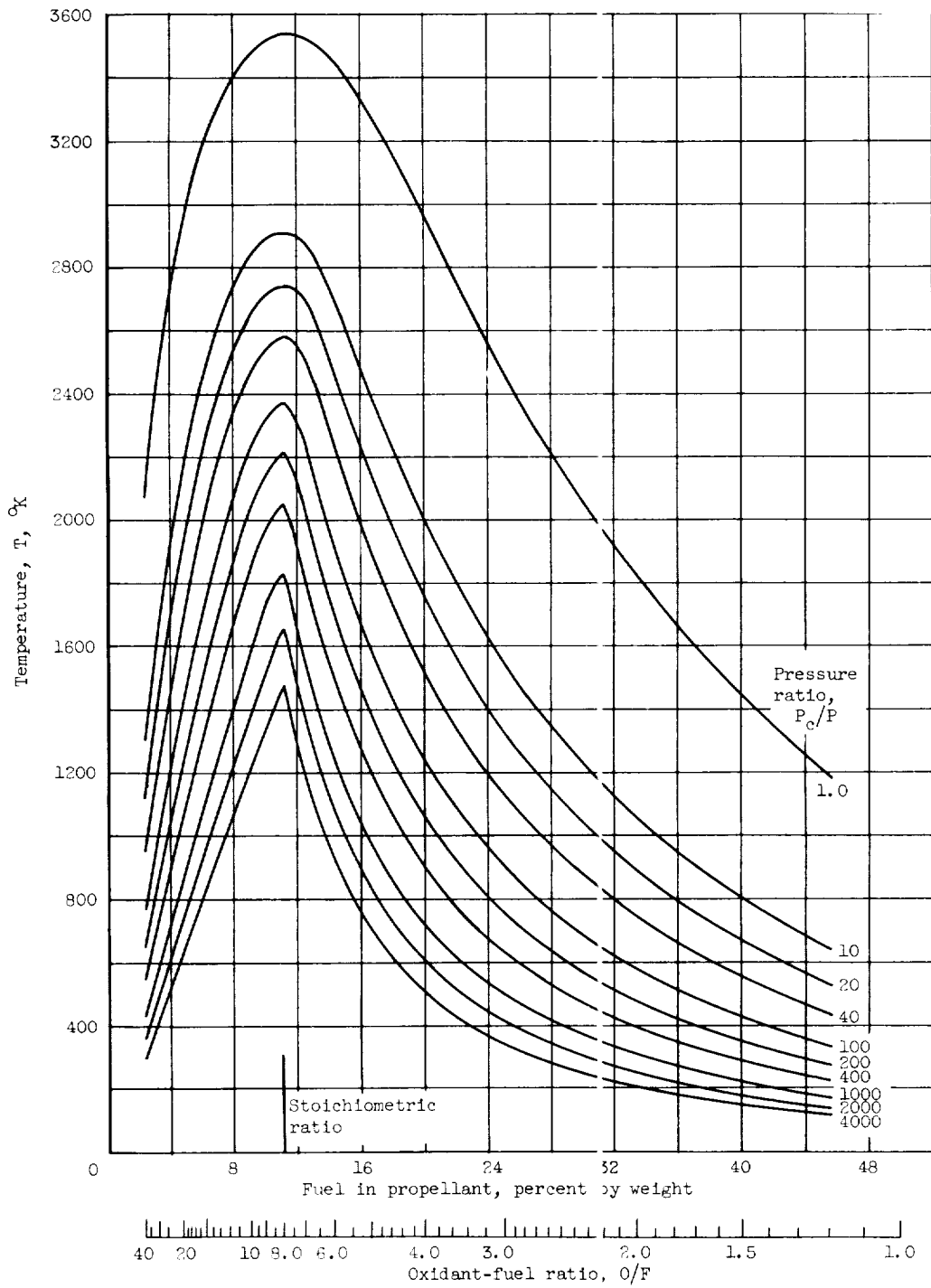
(f) Chamber pressure, 300 pounds per square inch absolute; equilibrium composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



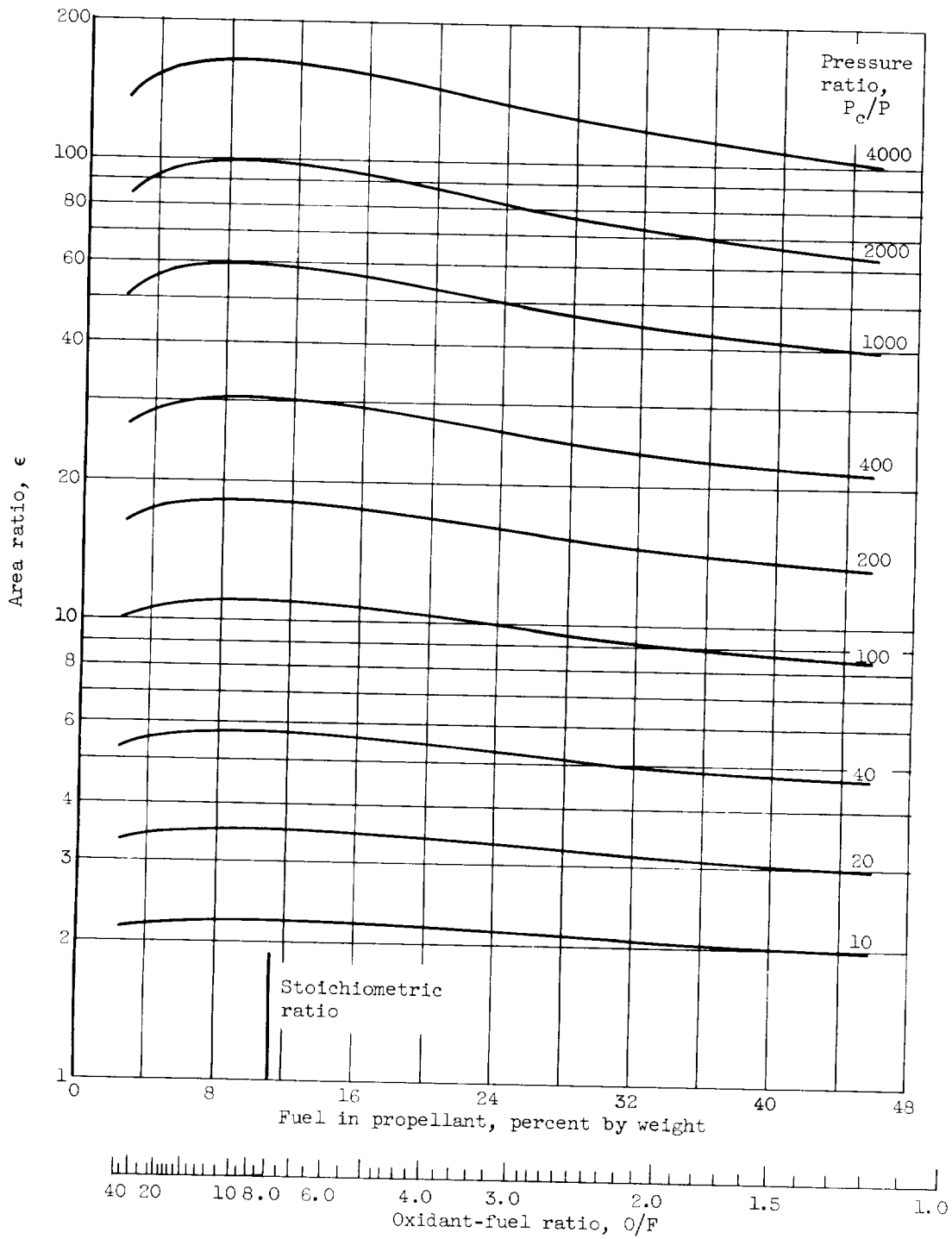
(g) Chamber pressure, 600 pounds per square inch absolute; frozen composition during expansion.

Figure 2. - Continued. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



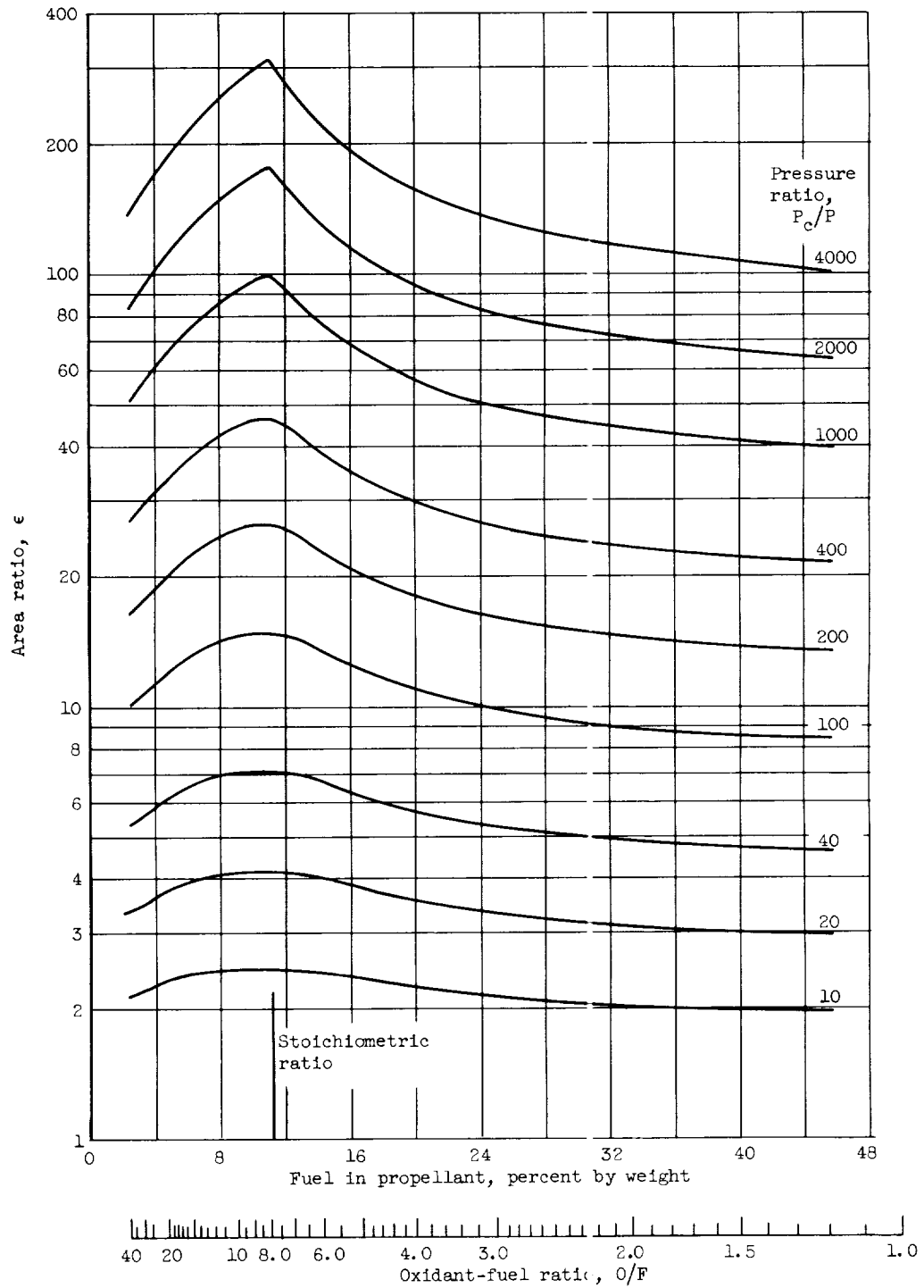
(h) Chamber pressure, 600 pounds per square inch absolute; equilibrium composition during expansion.

Figure 2. - Concluded. Theoretical combustion chamber and nozzle-exit temperatures of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



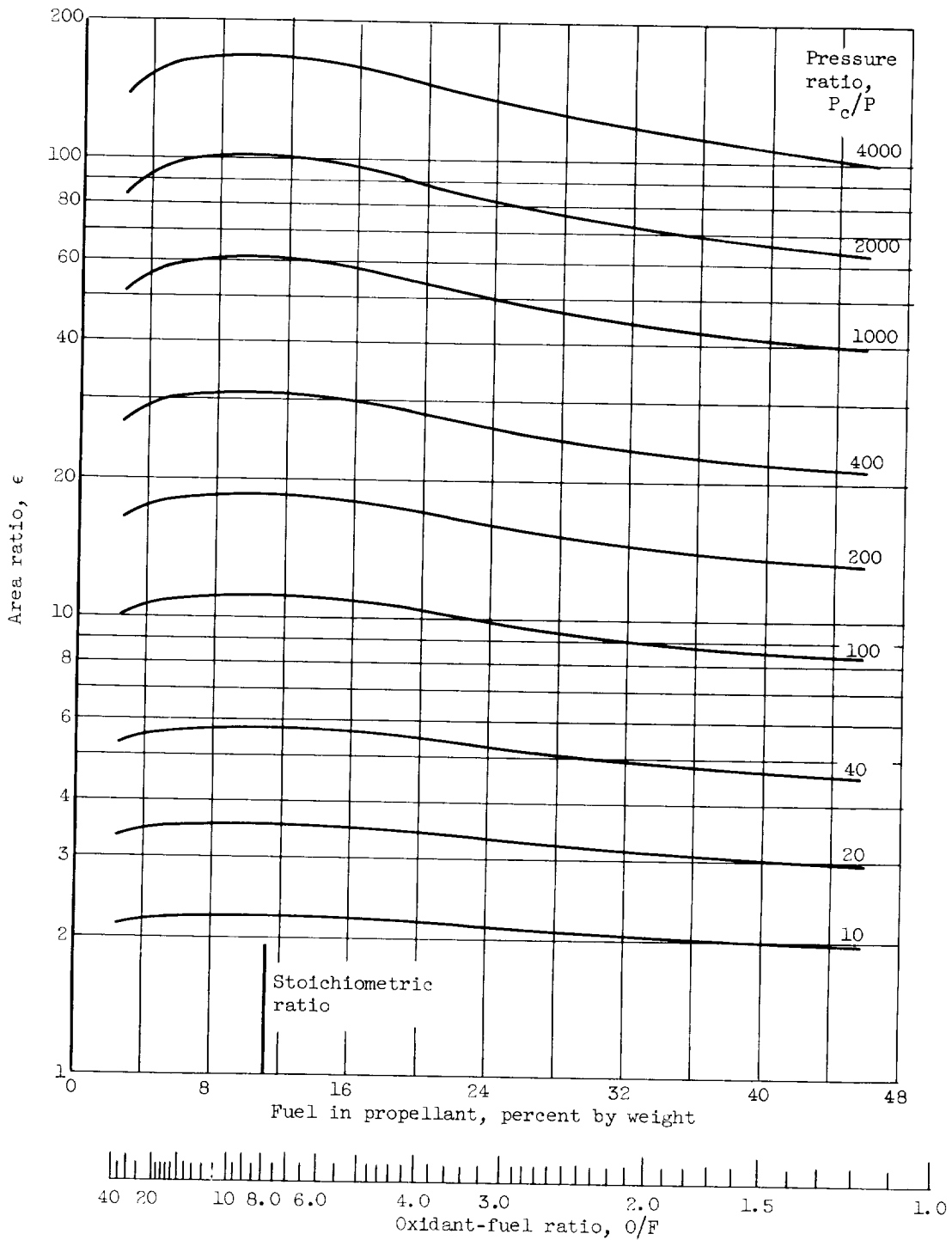
(a) Chamber pressure, 60 pounds per square inch absolute; frozen composition during expansion.

Figure 3. - Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



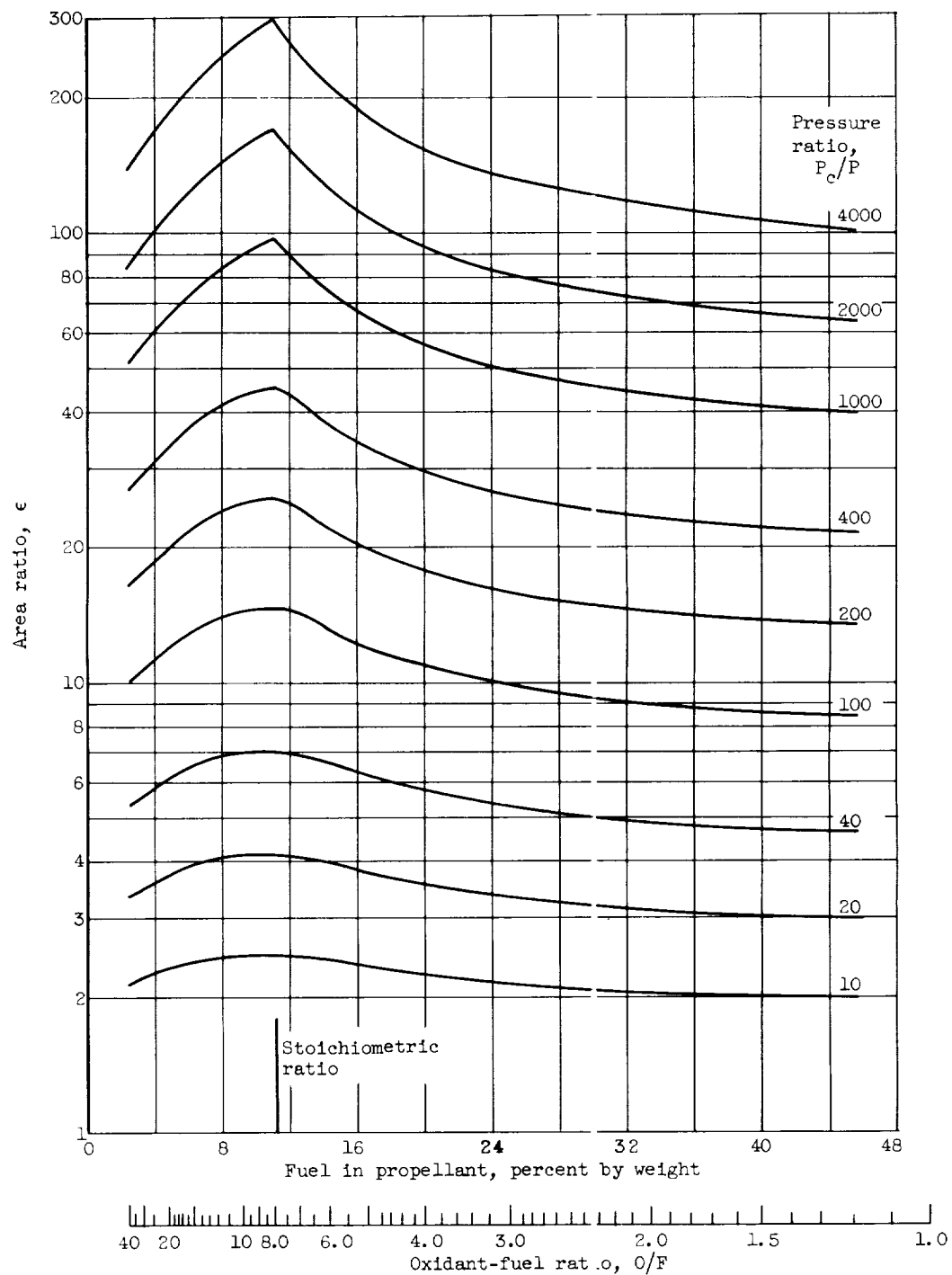
(b) Chamber pressure, 60 pounds per square inch absolute; equilibrium composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



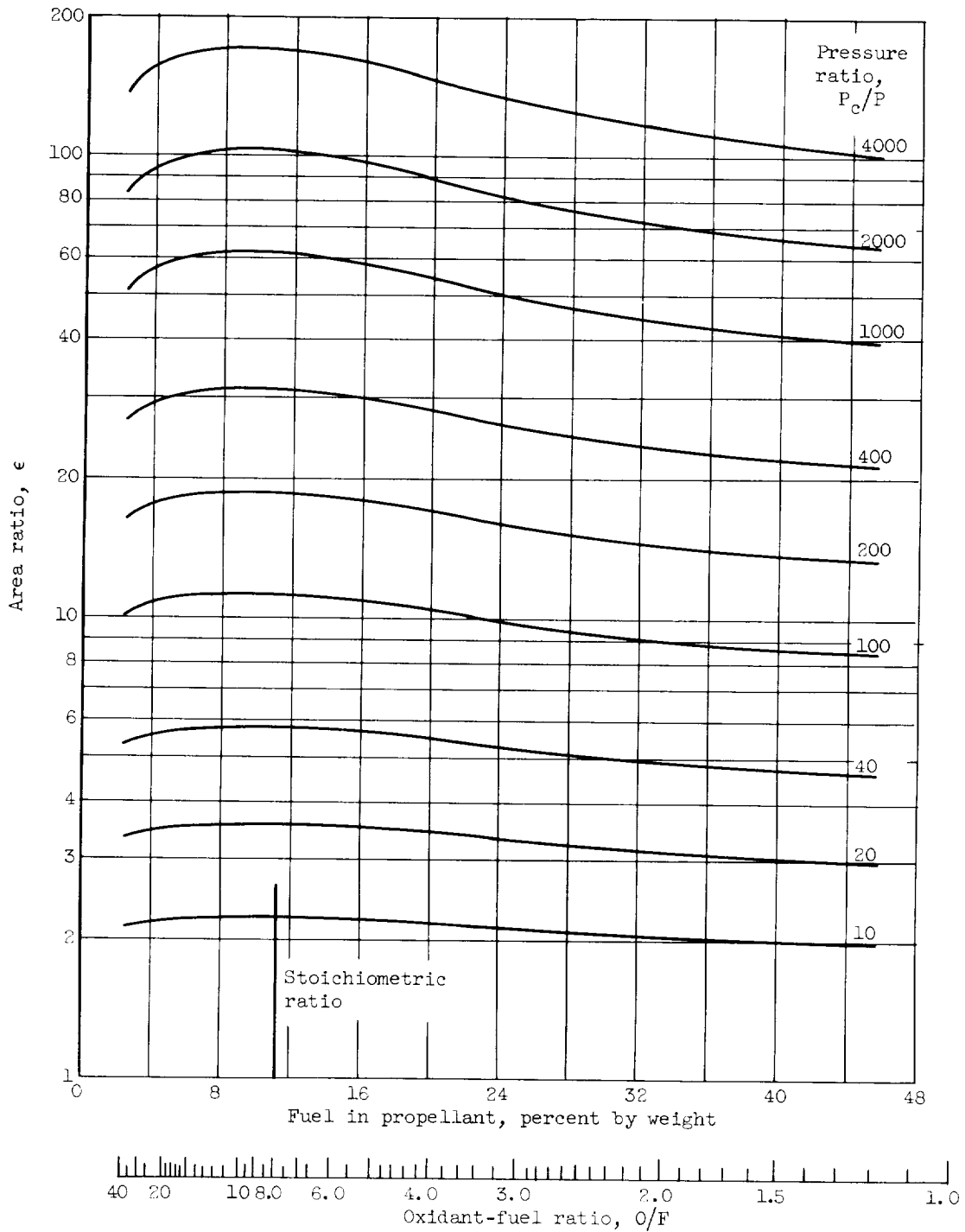
(c) Chamber pressure, 150 pounds per square inch absolute; frozen composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



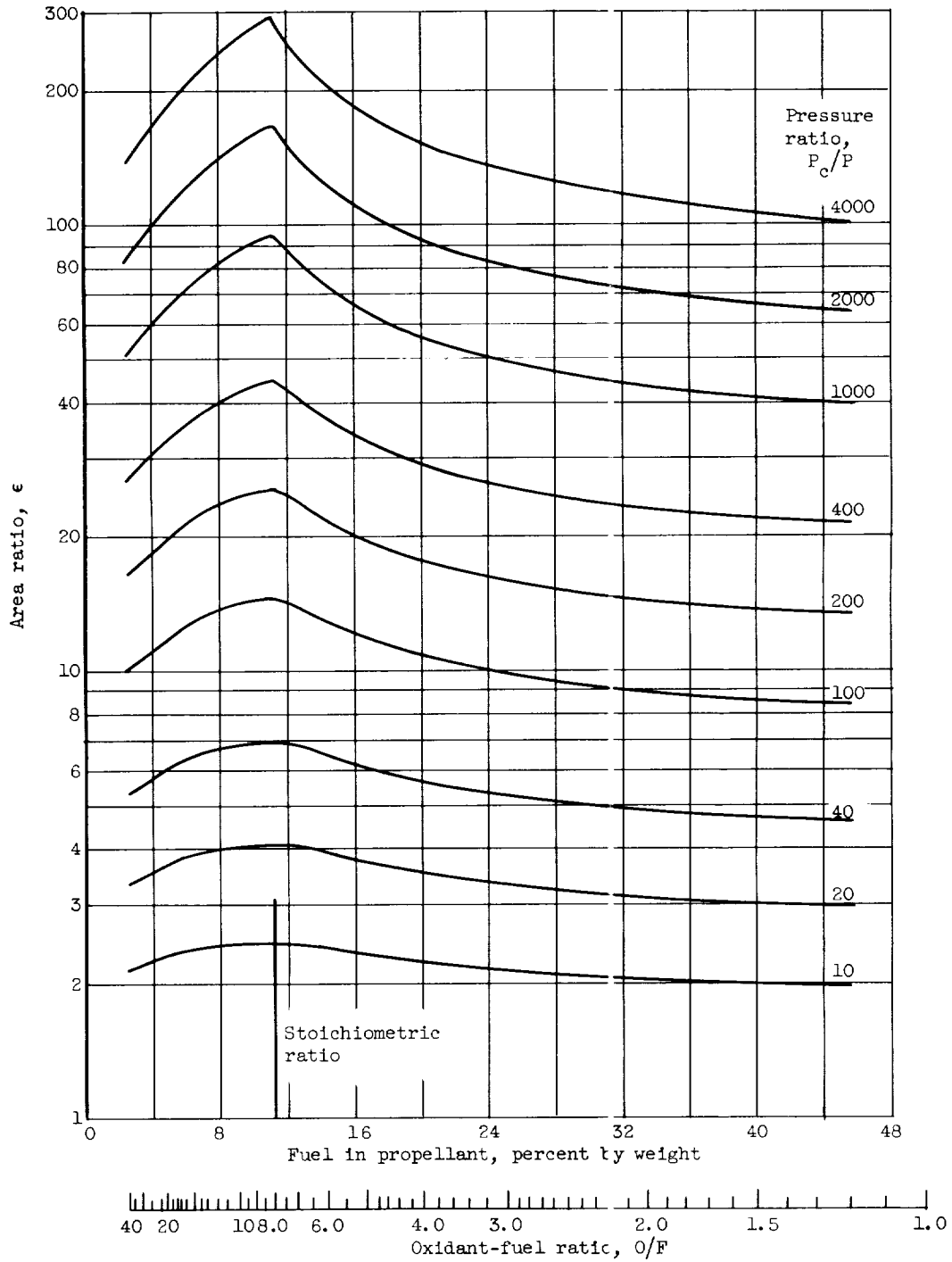
(d) Chamber pressure, 150 pounds per square inch absolute; equilibrium composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



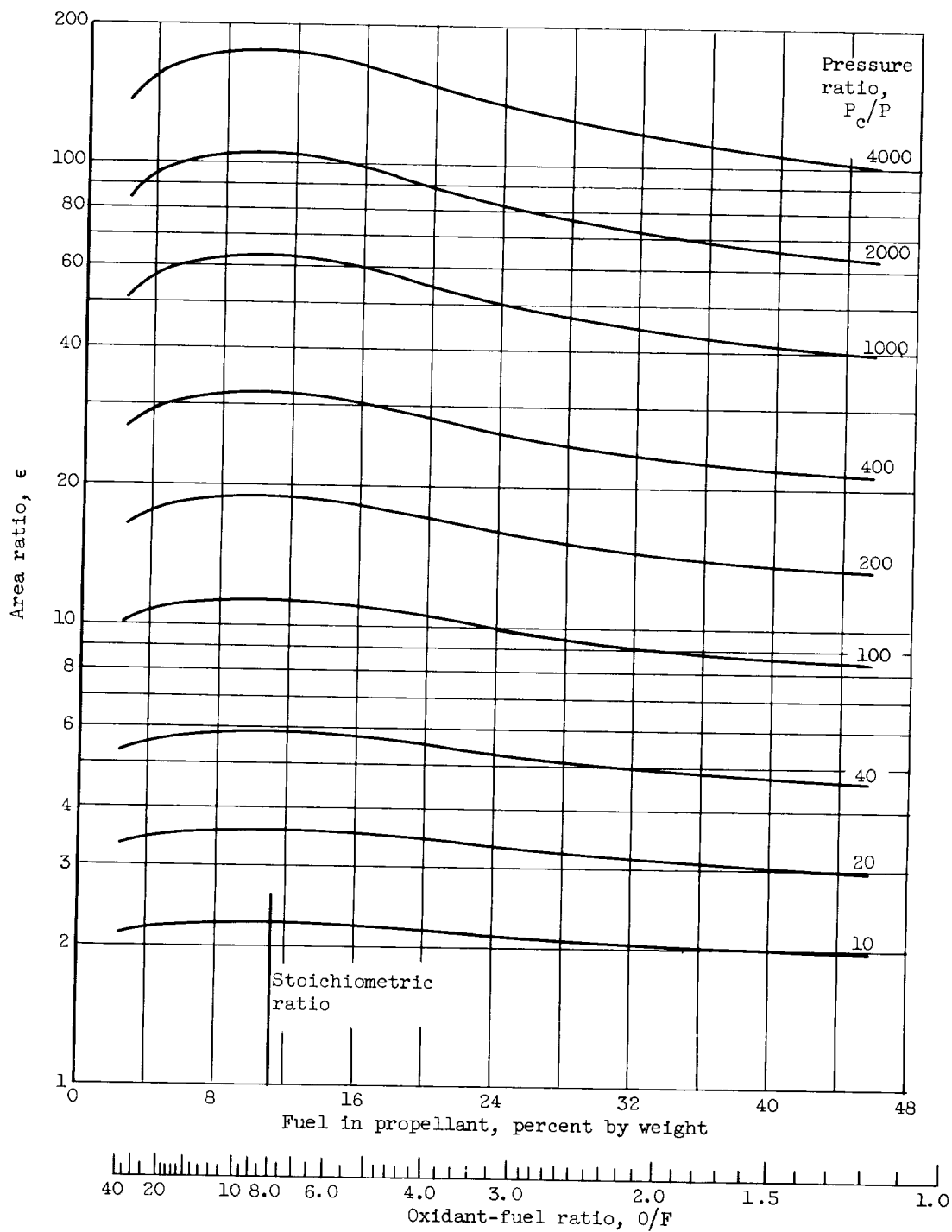
(e) Chamber pressure, 300 pounds per square inch absolute; frozen composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



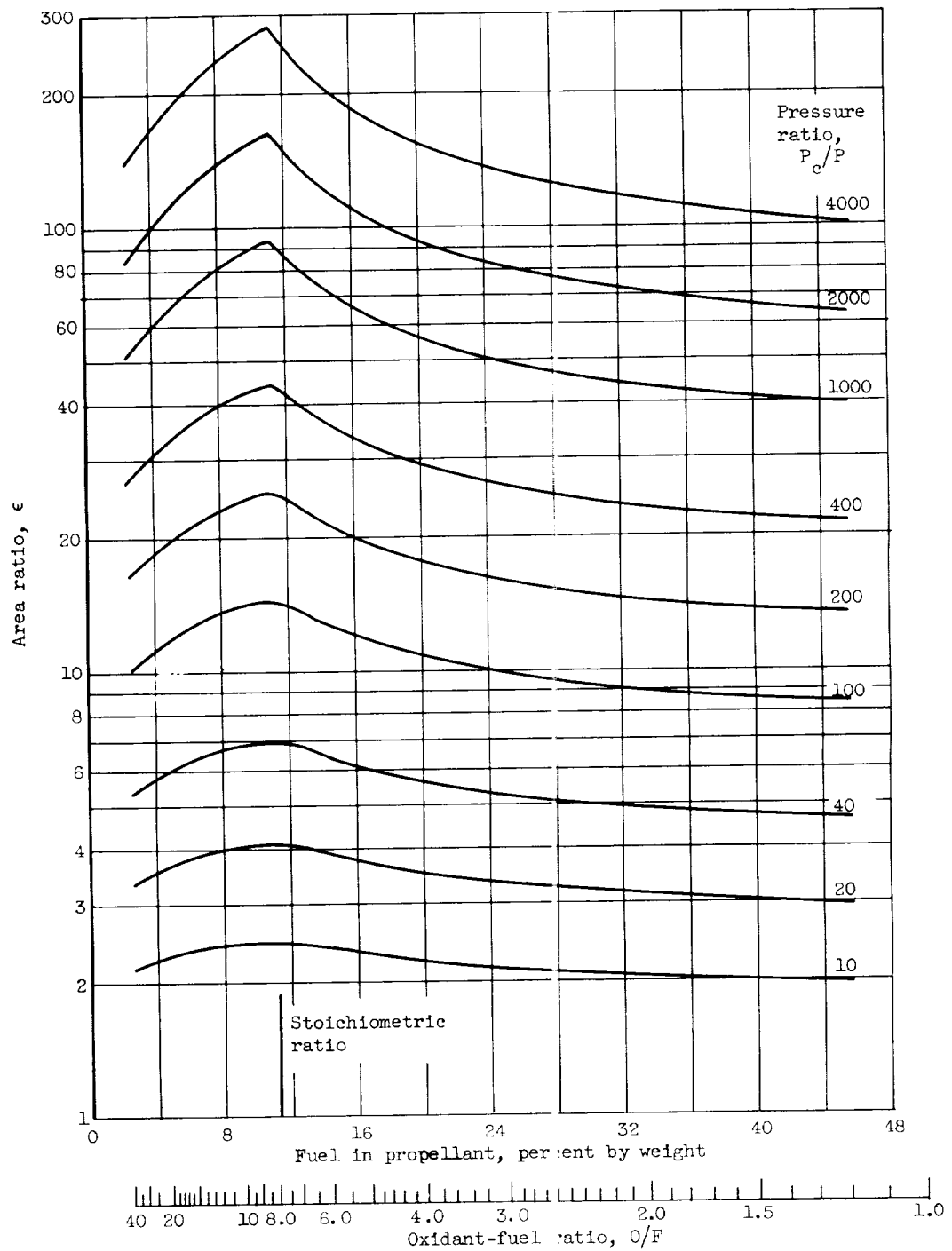
(f) Chamber pressure, 300 pounds per square inch absolute; equilibrium composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



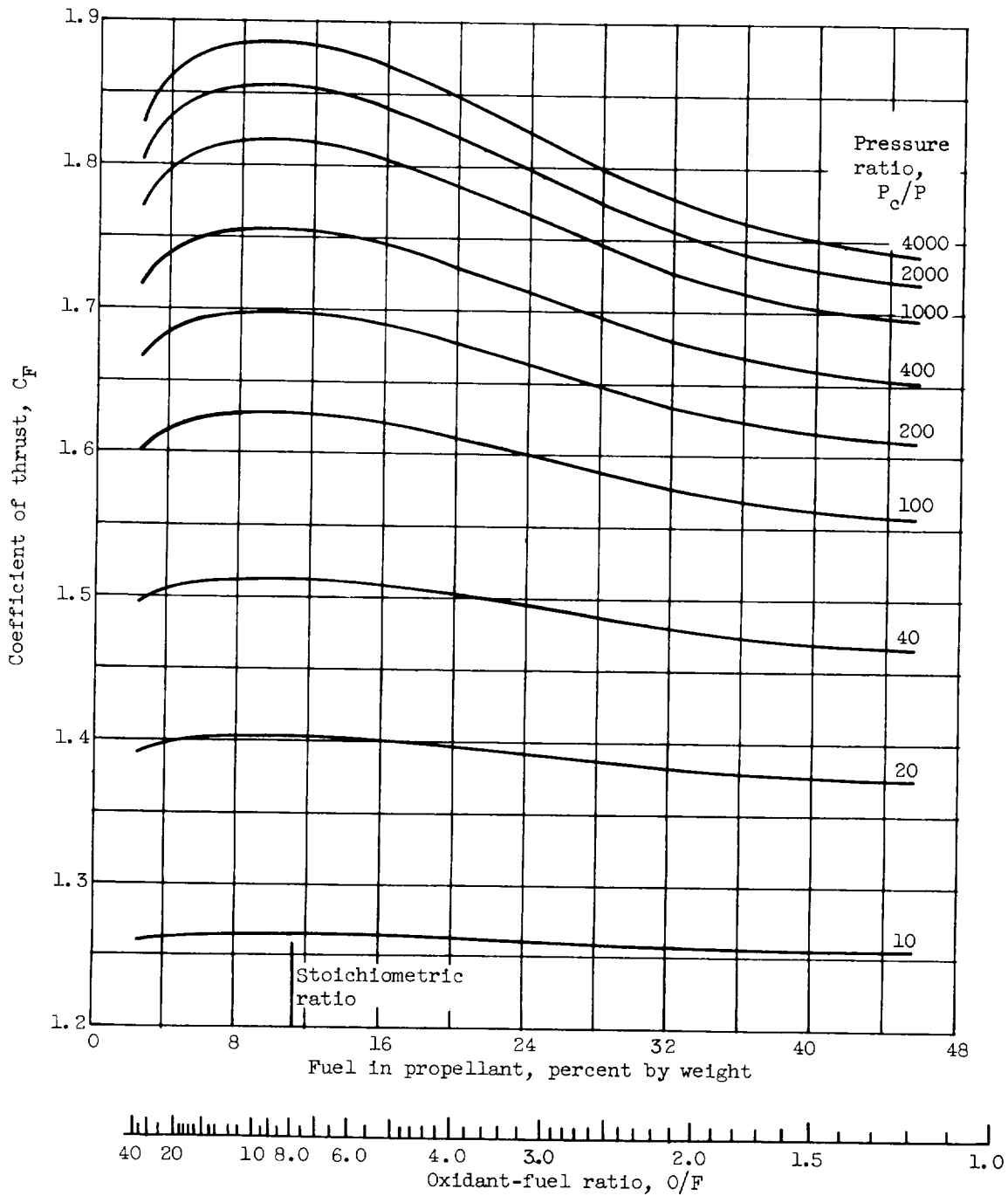
(g) Chamber pressure, 600 pounds per square inch absolute; frozen composition during expansion.

Figure 3. - Continued. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



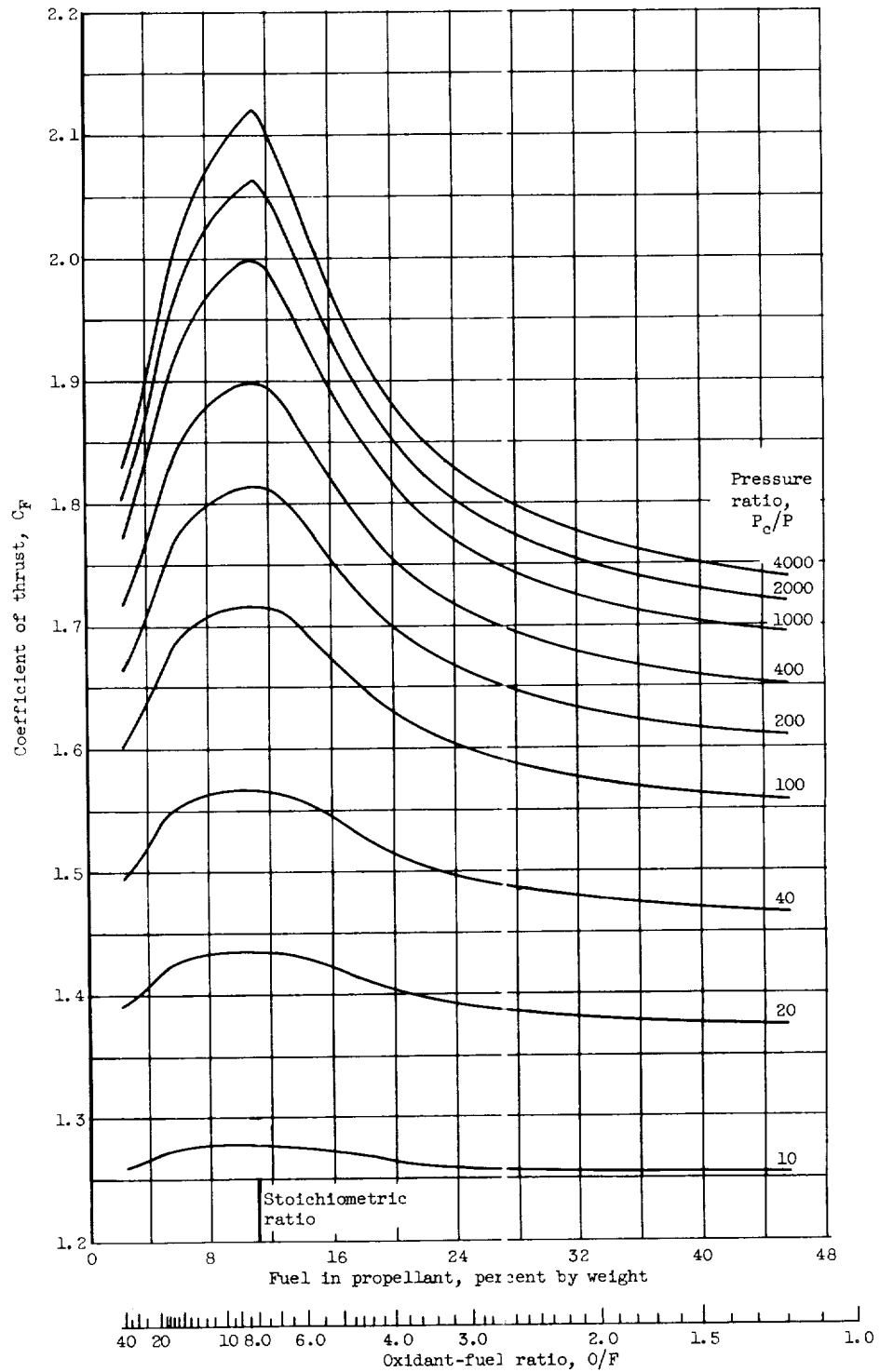
(h) Chamber pressure, 600 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 3. - Concluded. Theoretical ratio of nozzle area to throat area for liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



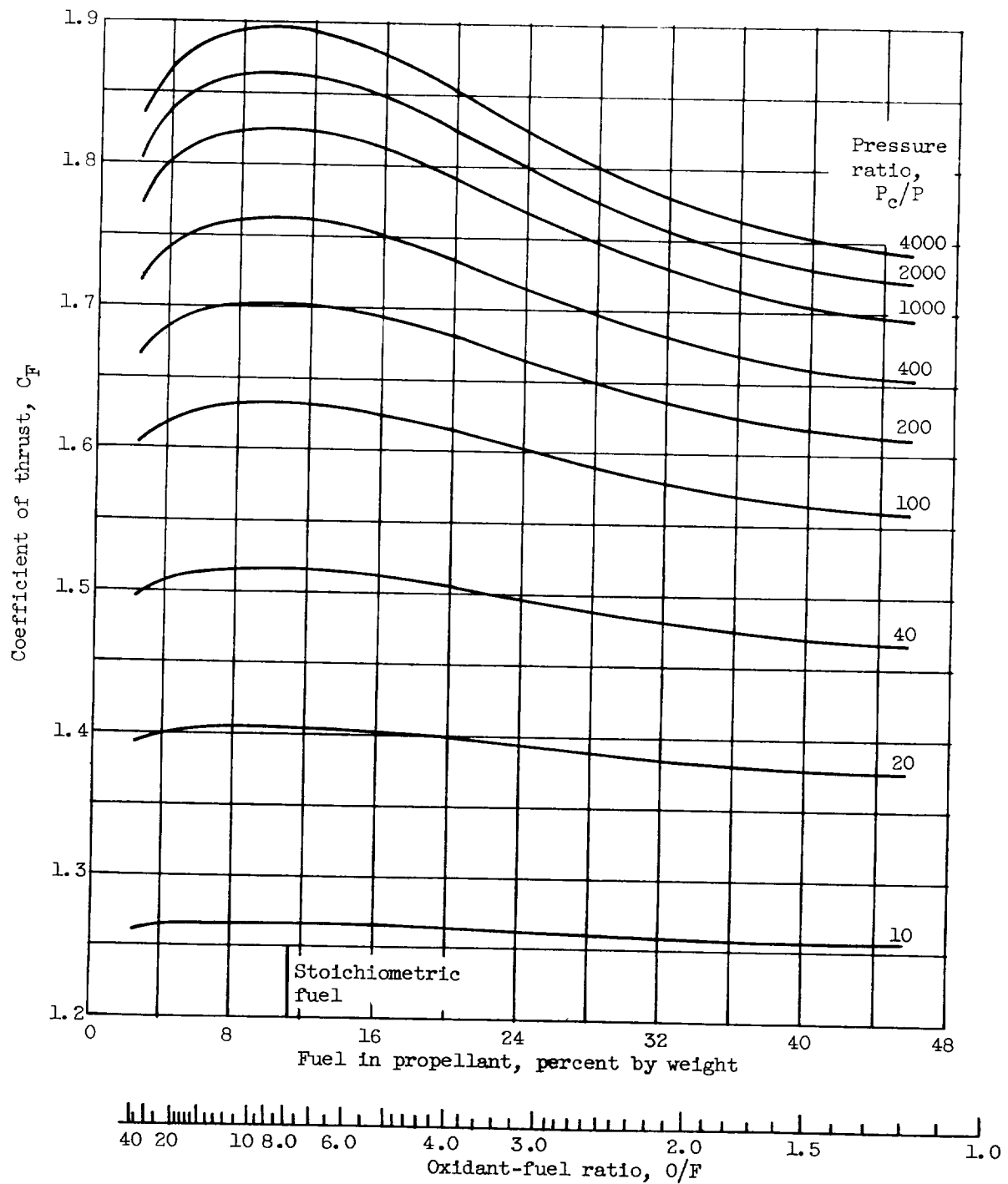
(a) Chamber pressure, 60 pounds per square inch absolute;
frozen composition during expansion.

Figure 4. - Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



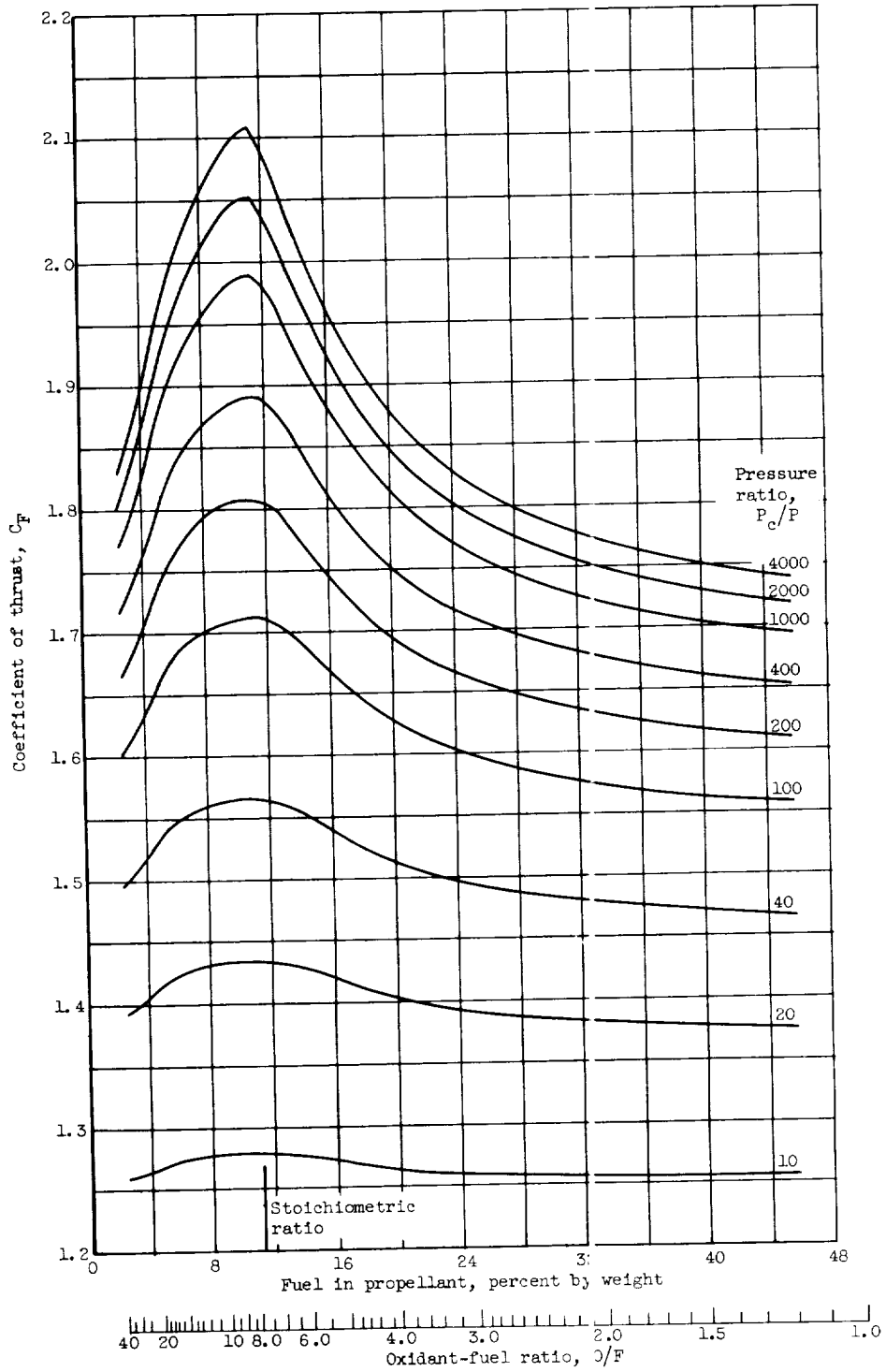
(b) Chamber pressure, 60 pounds per square inch absolute; equilibrium composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



(c) Chamber pressure, 150 pounds per square inch absolute;
frozen composition during expansion.

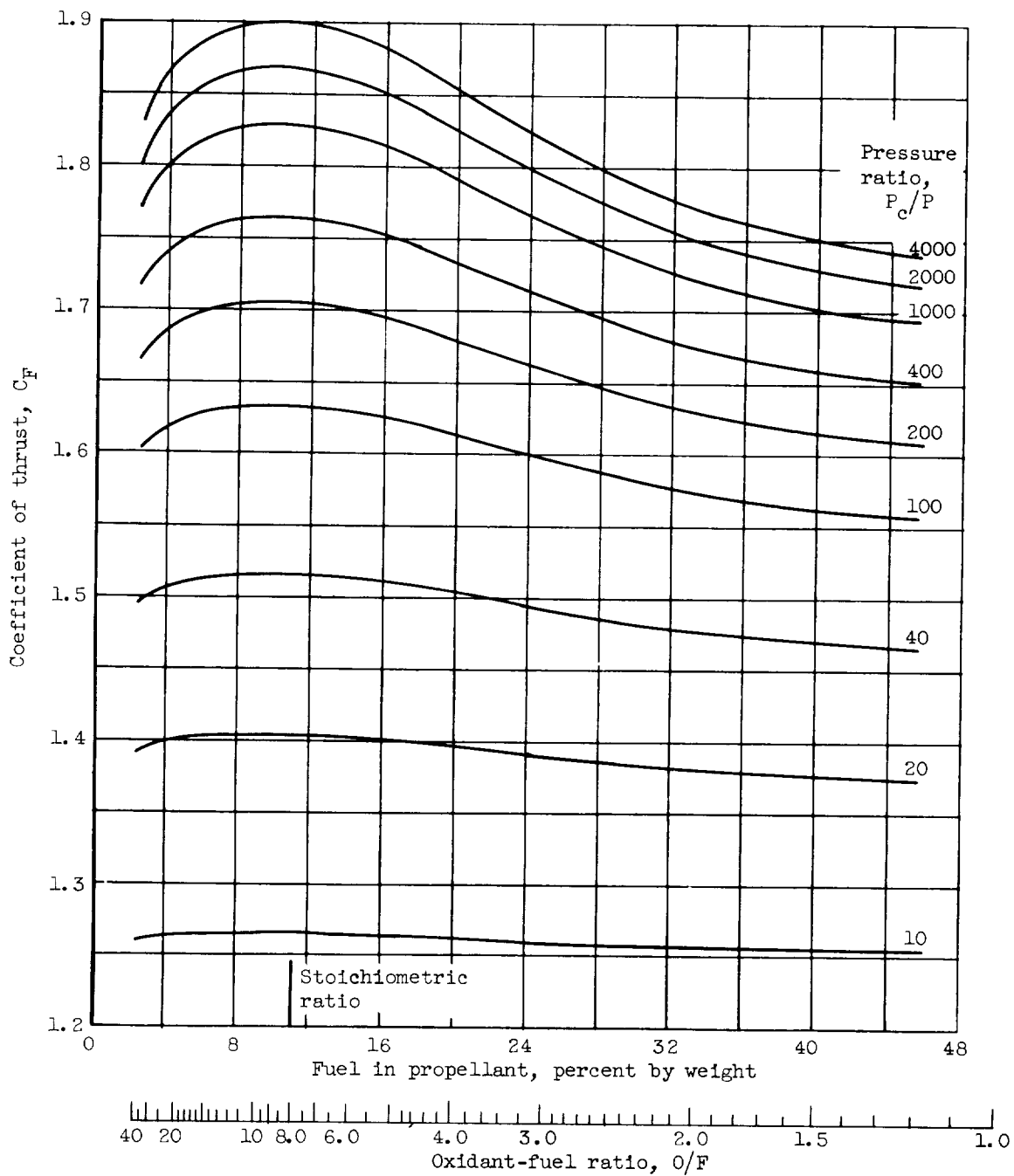
Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



(d) Chamber pressure, 150 pounds per square inch absolute; equilibrium composition during expansion.

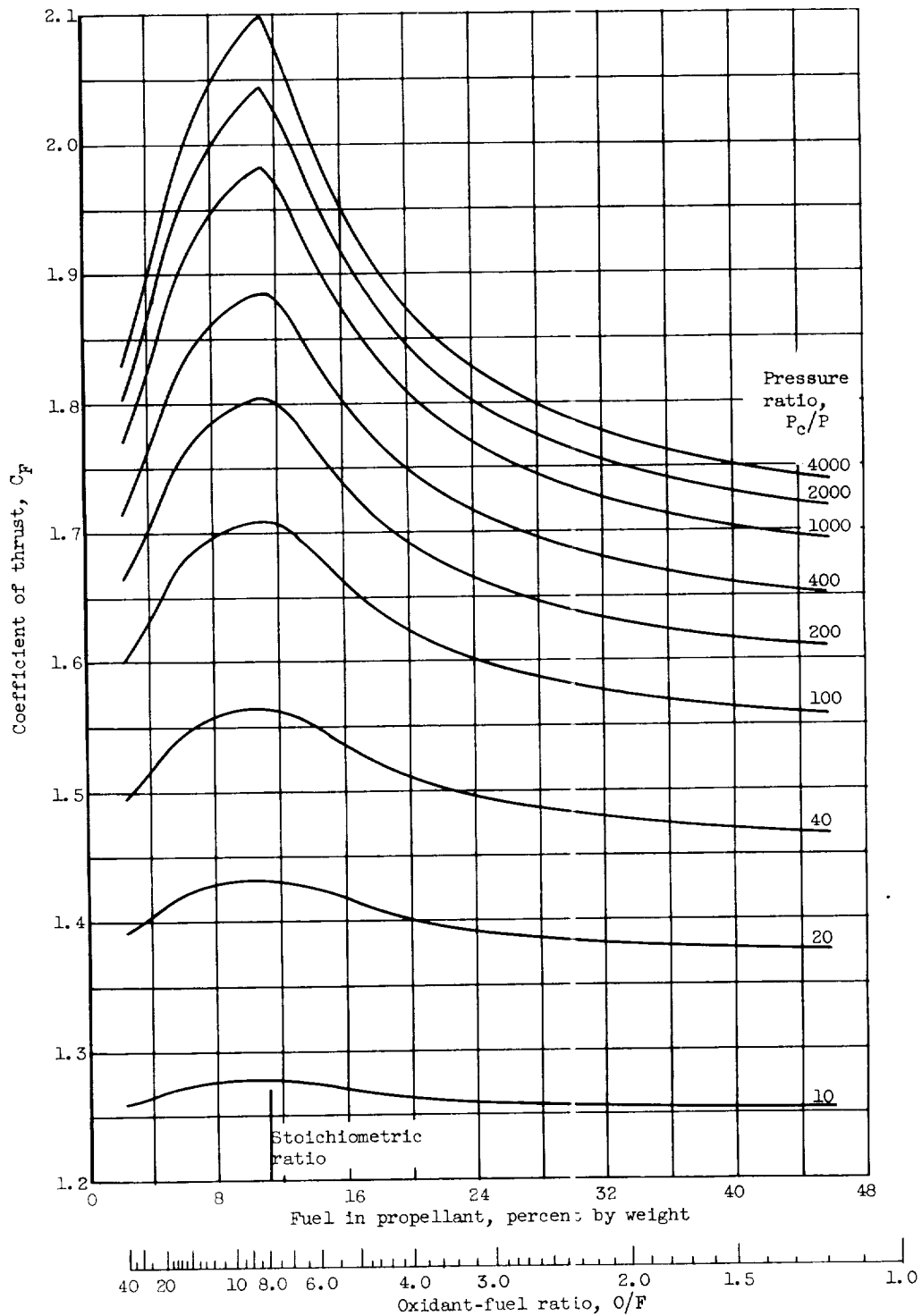
Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.

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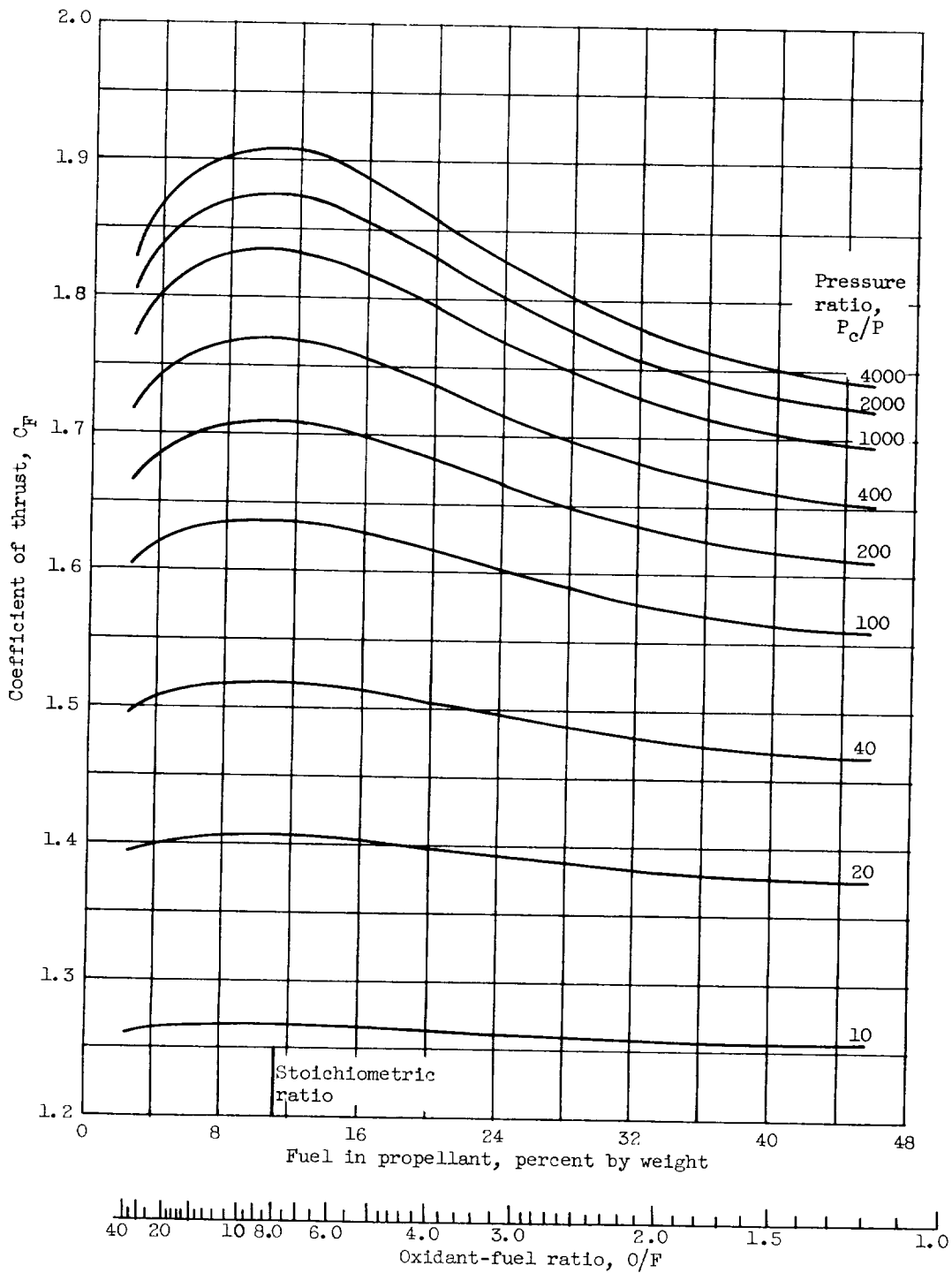
(e) Chamber pressure, 300 pounds per square inch absolute;
frozen composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



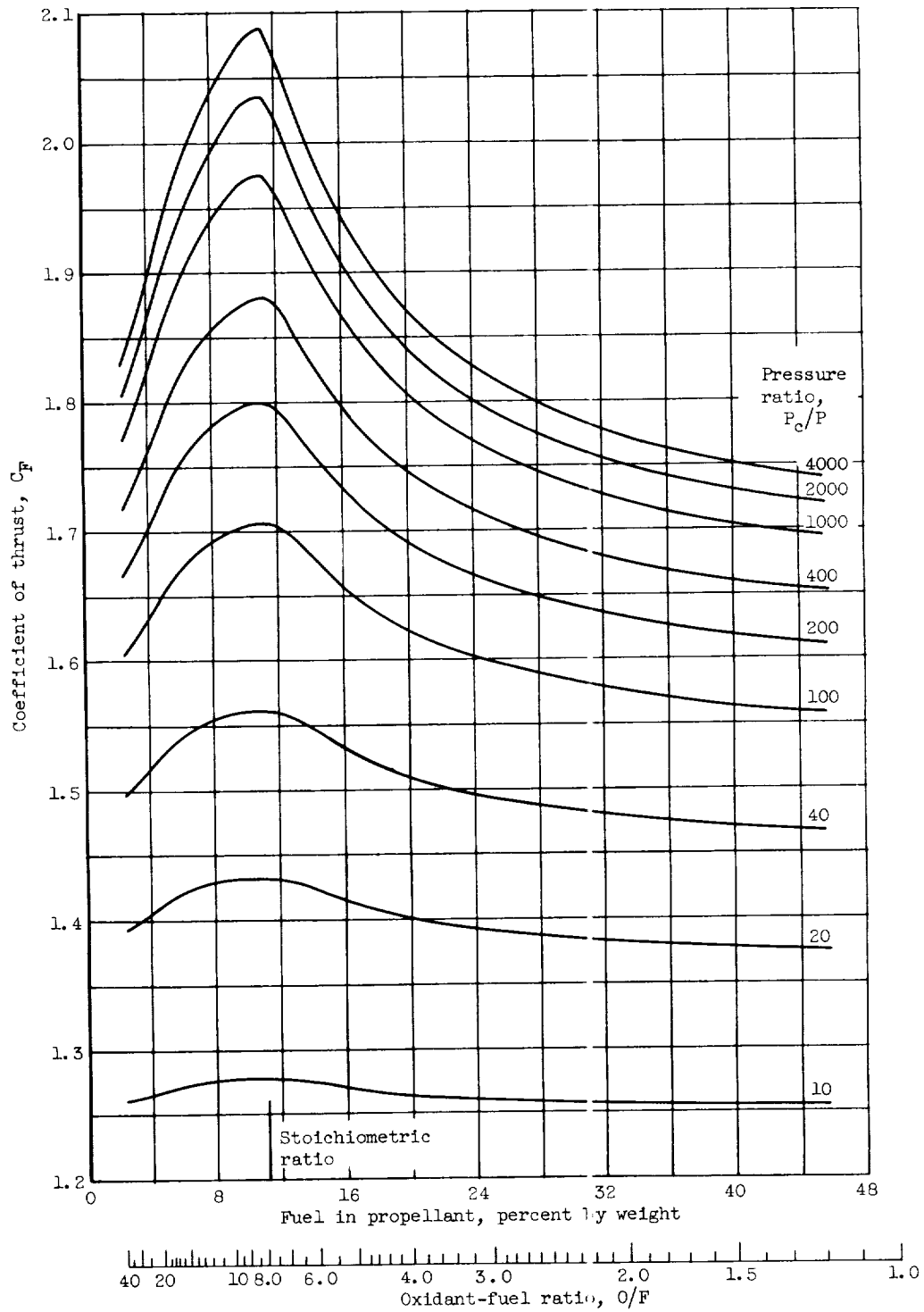
(f) Chamber pressure, 300 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



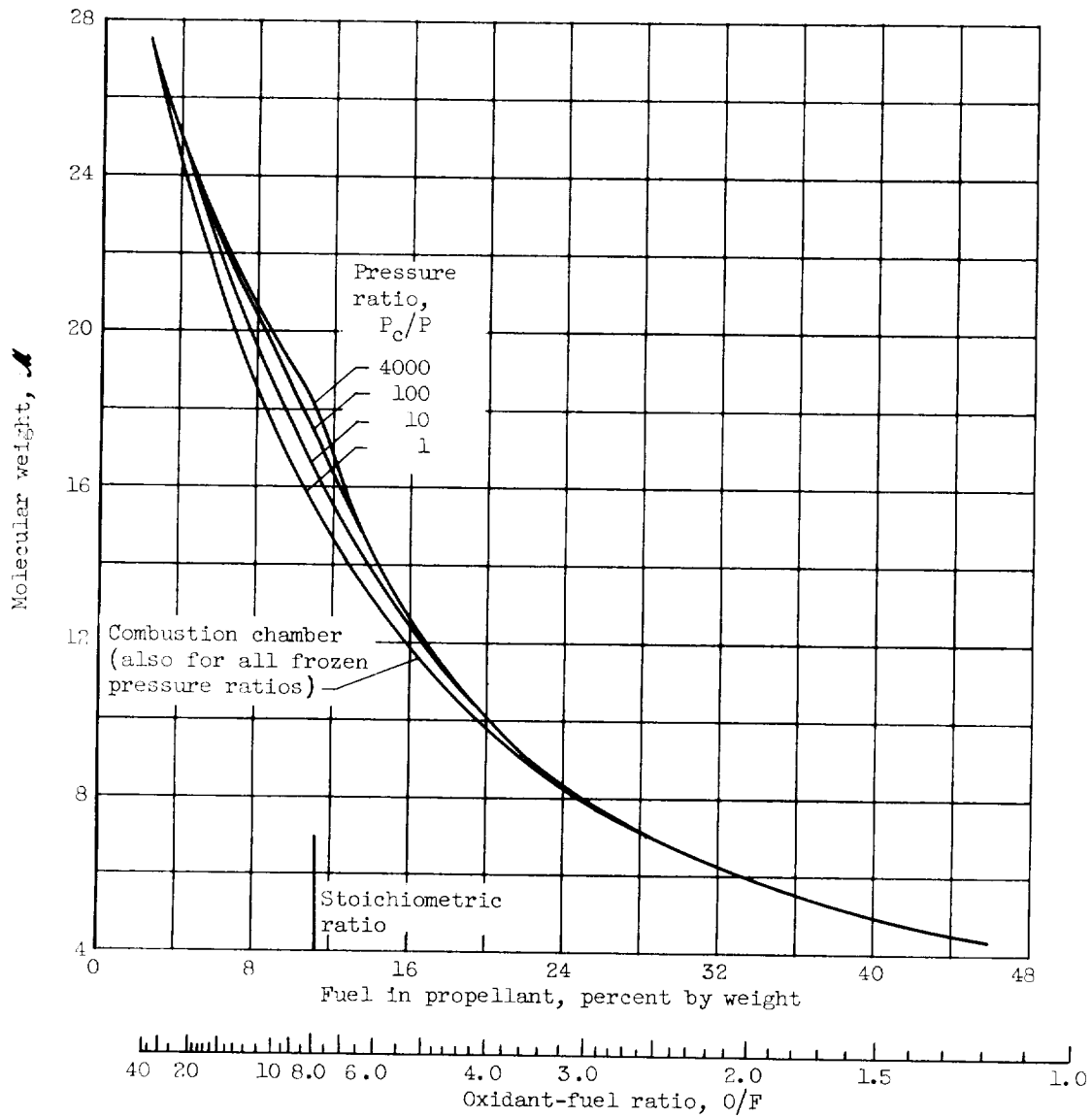
(g) Chamber pressure, 600 pounds per square inch absolute;
frozen composition during expansion.

Figure 4. - Continued. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



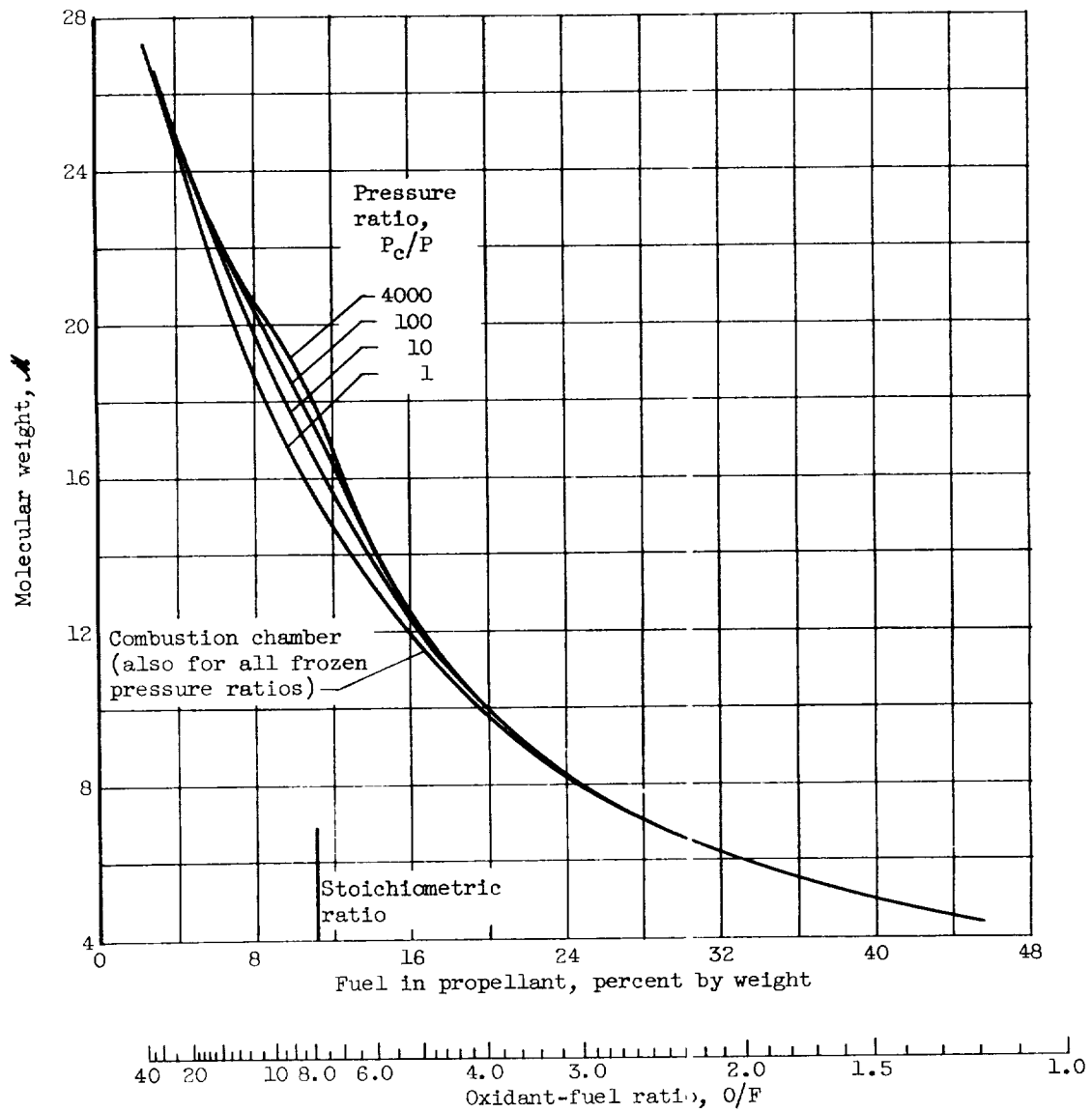
(h) Chamber pressure, 600 pounds per square inch absolute; equilibrium composition during expansion.

Figure 4. - Concluded. Theoretical coefficient of thrust of liquid hydrogen and liquid oxygen. Isentropic expansion to pressure ratio indicated.



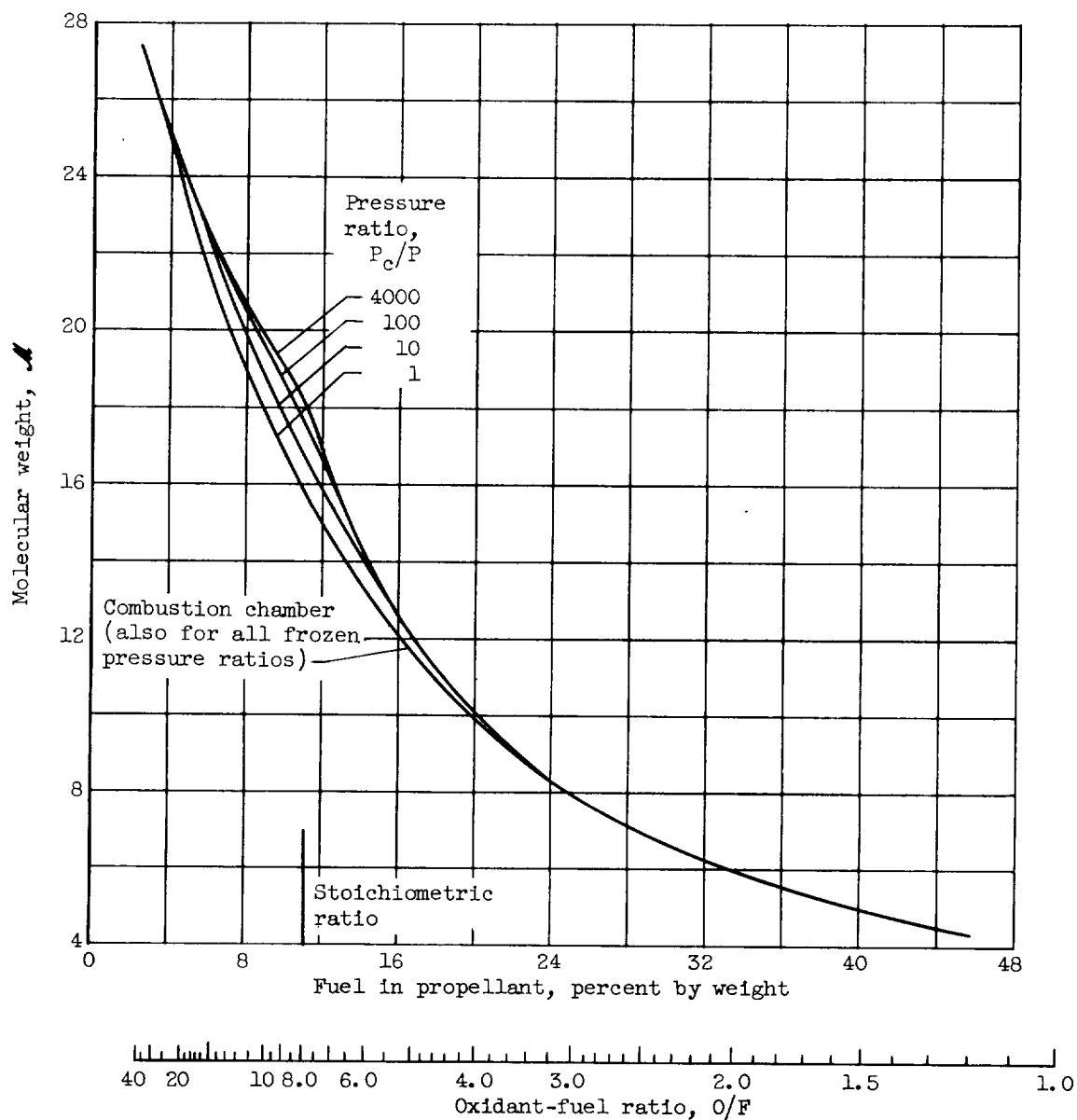
(a) Chamber pressure, 60 pounds per square inch absolute.

Figure 5. - Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



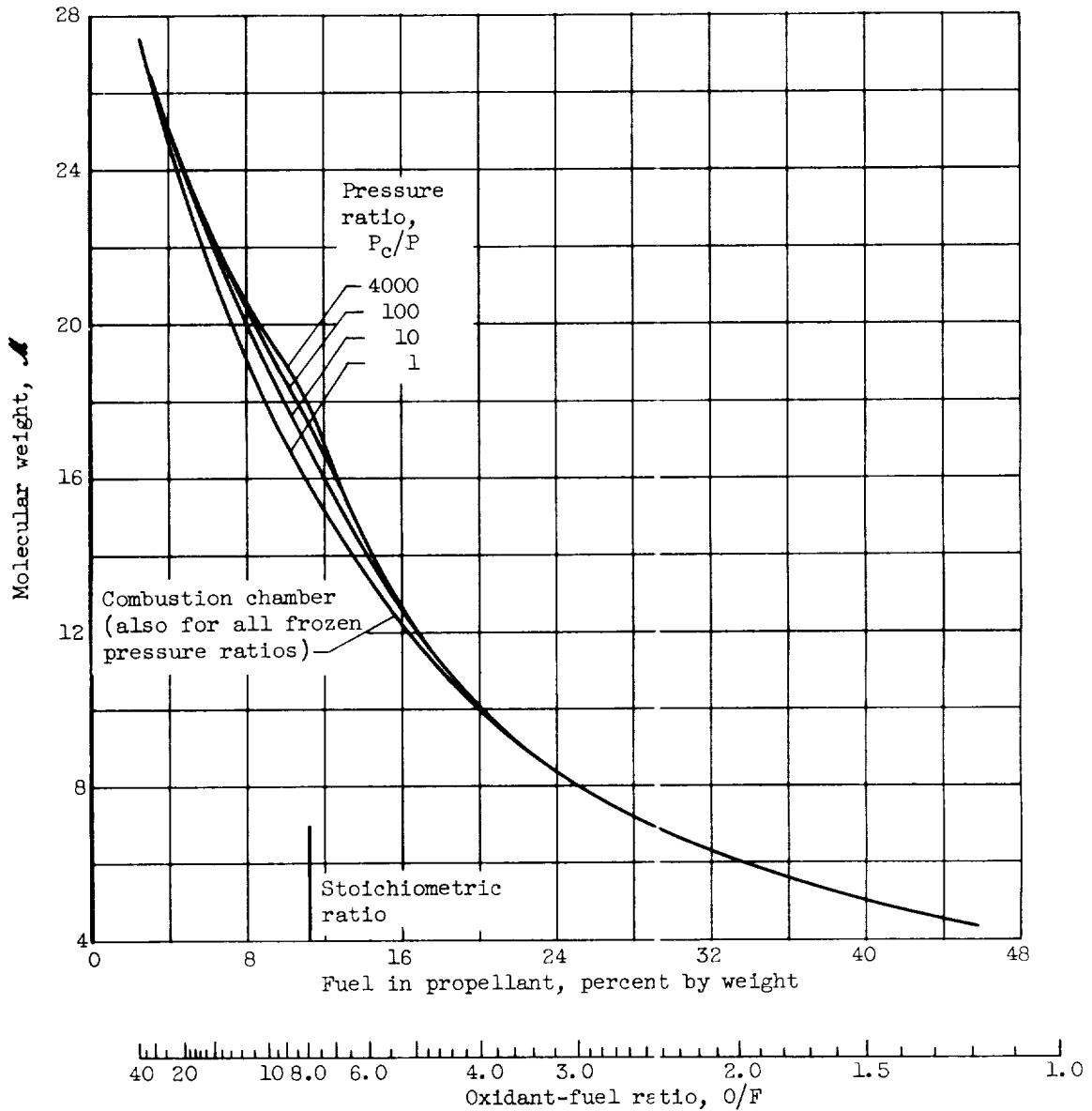
(b) Chamber pressure, 150 pounds per square inch absolute.

Figure 5. - Continued. Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



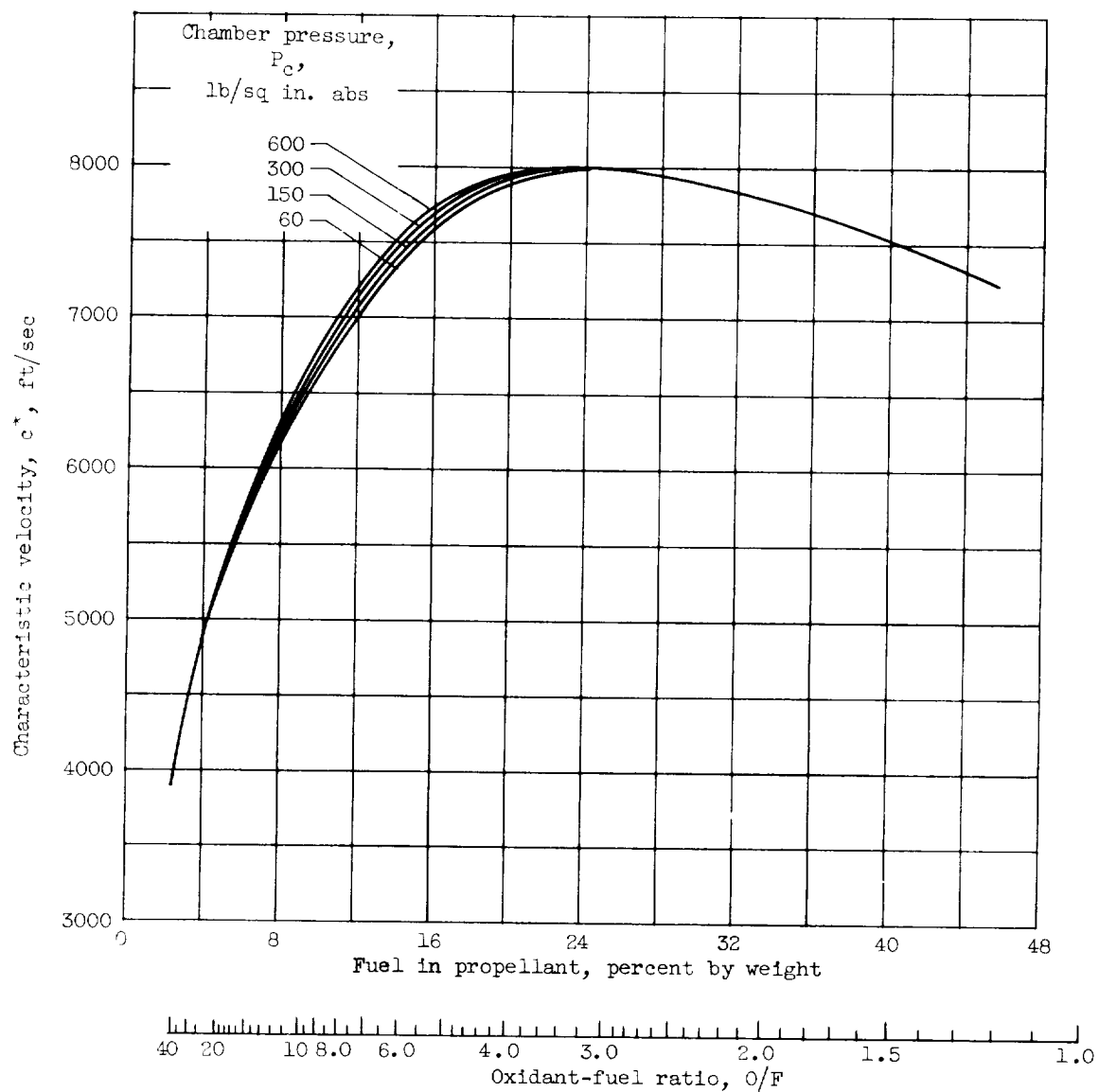
(c) Chamber pressure, 300 pounds per square inch absolute.

Figure 5. - Continued. Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



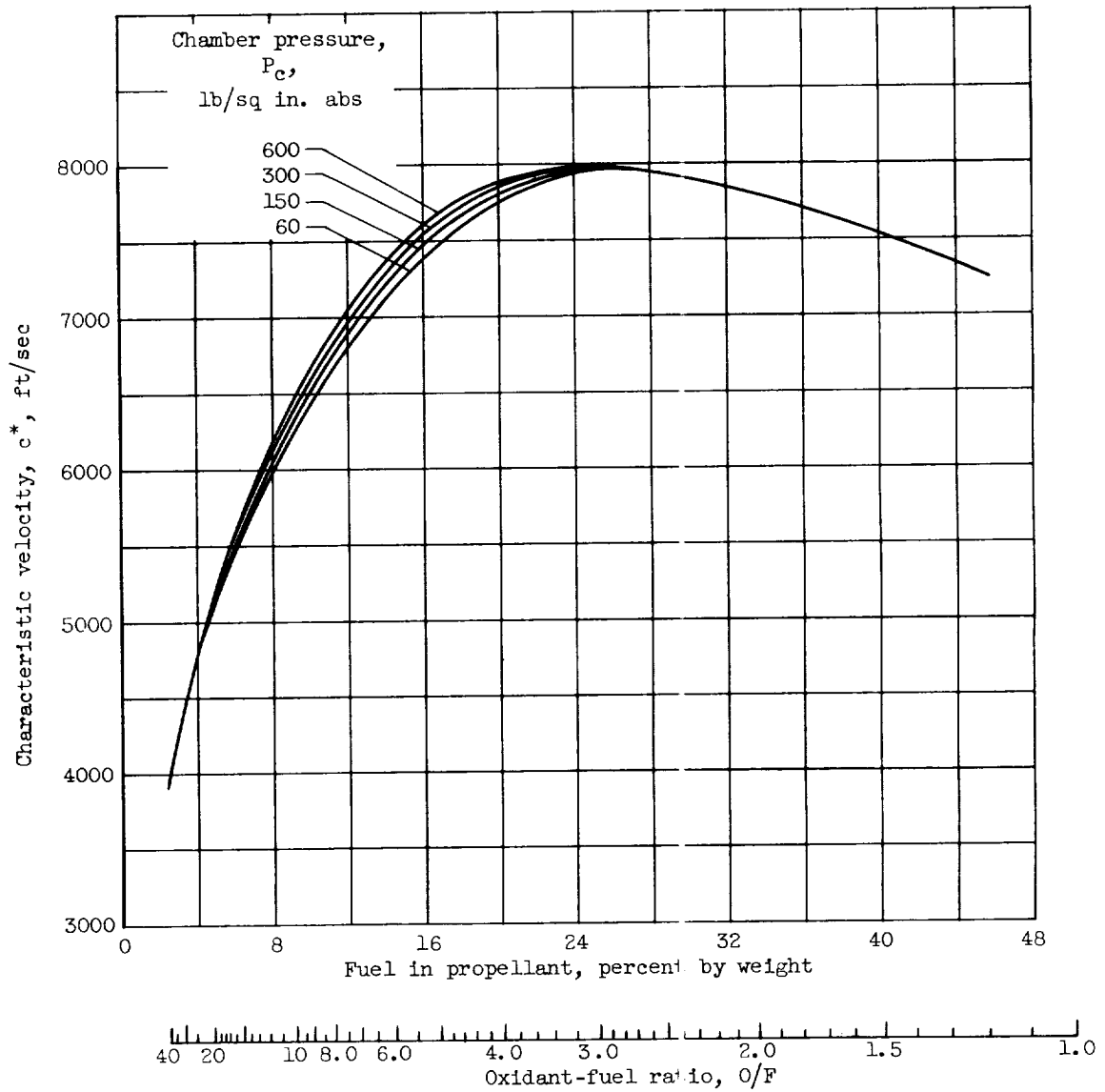
(d) Chamber pressure, 600 pounds per square inch absolute.

Figure 5. - Concluded. Theoretical molecular weight of liquid hydrogen and liquid oxygen. Equilibrium composition during isentropic expansion to pressure ratio indicated.



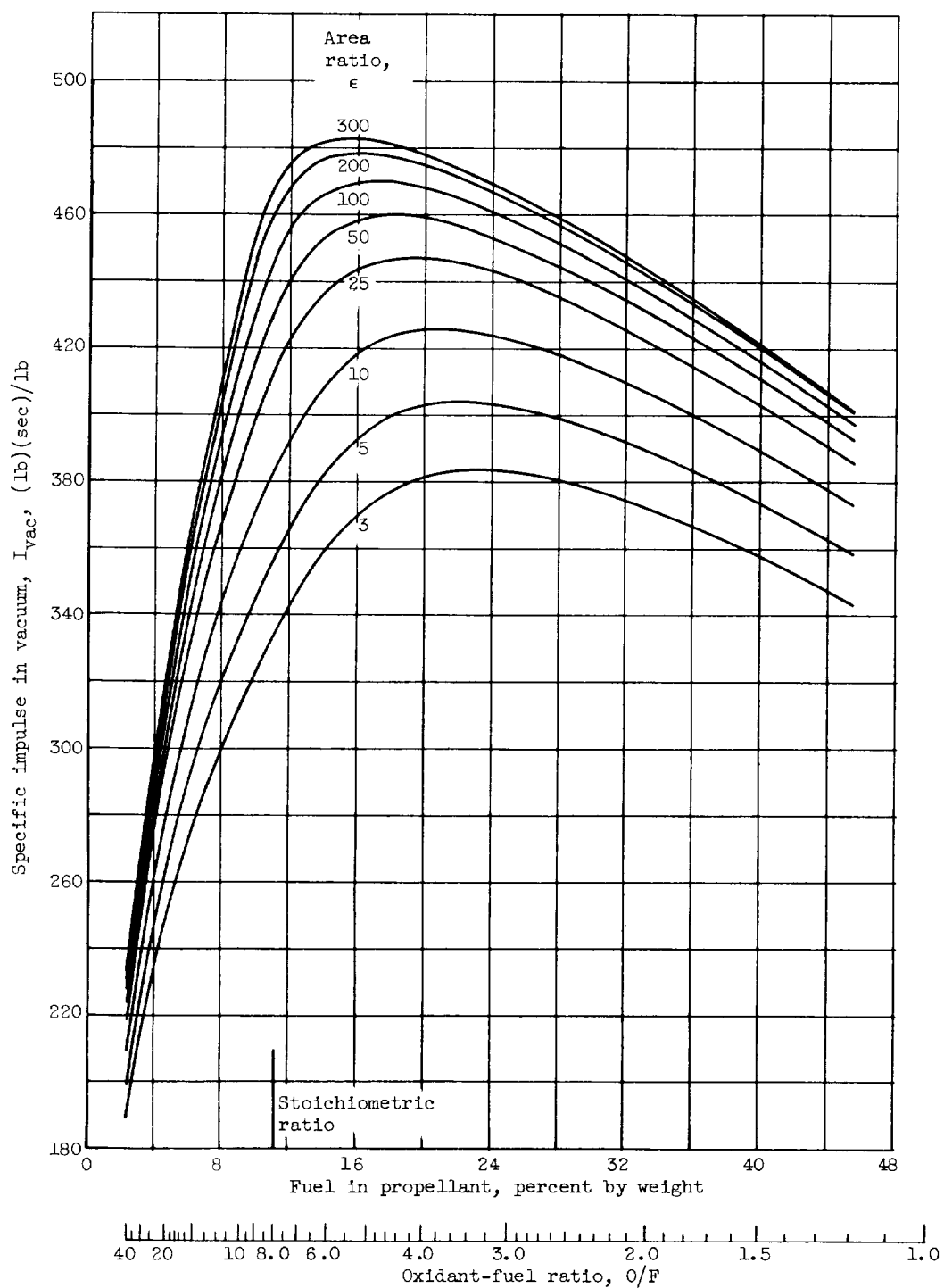
(a) Equilibrium composition during expansion.

Figure 6. - Theoretical characteristic velocity of liquid hydrogen and liquid oxygen.



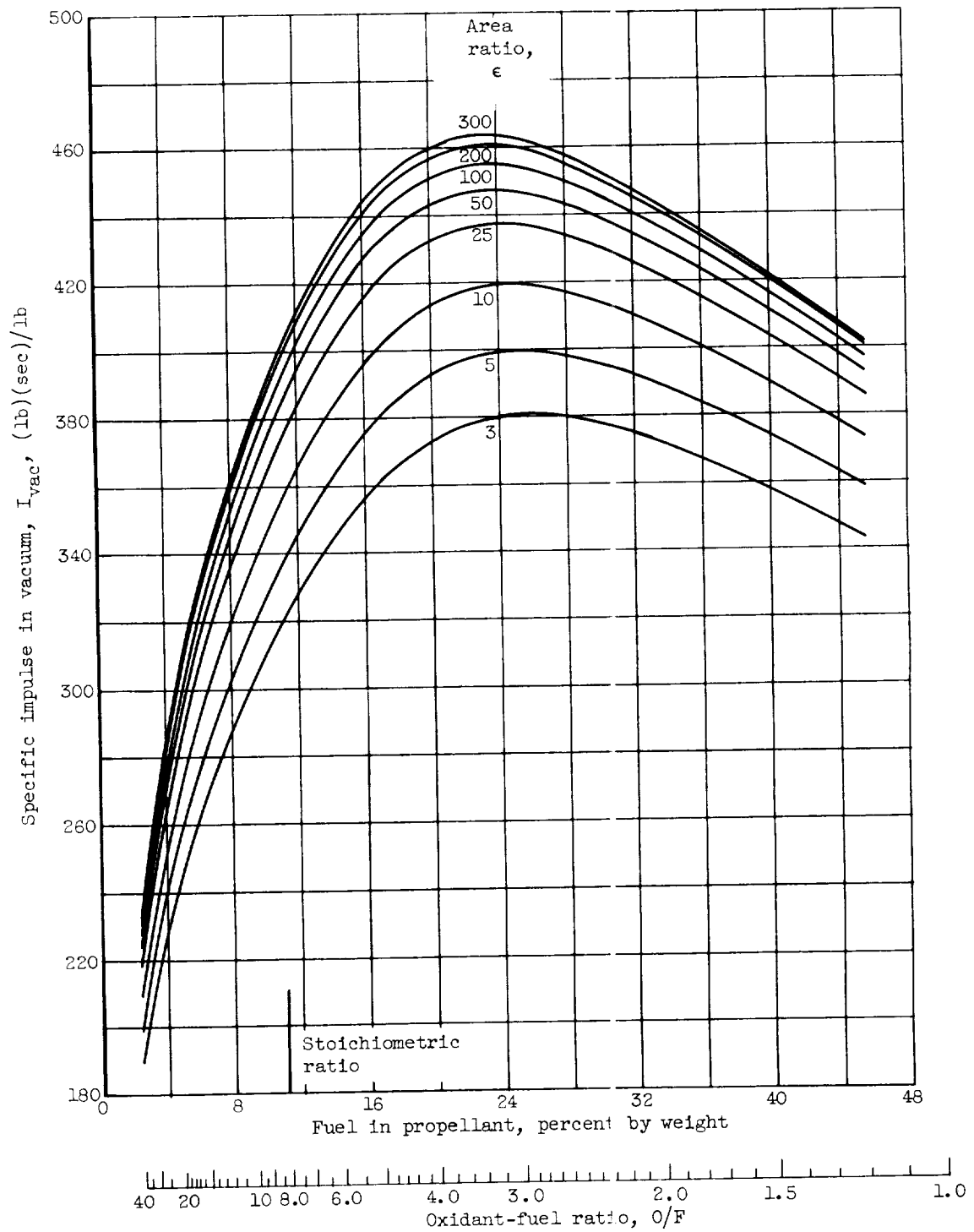
(b) Frozen composition during expansion.

Figure 6. - Concluded. Theoretical characteristic velocity of liquid hydrogen and liquid oxygen.



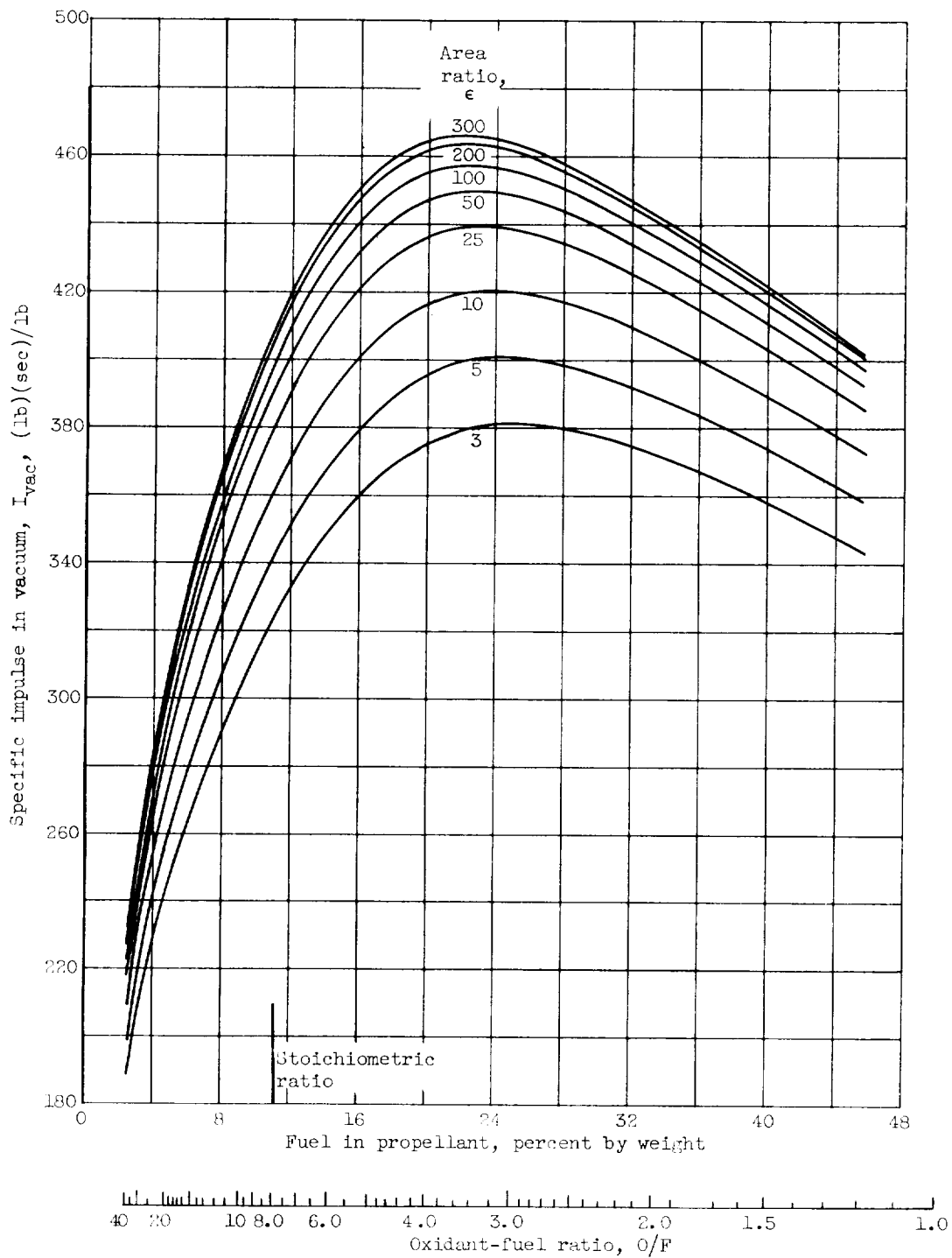
(b) Chamber pressure, 60 pounds per square inch absolute;
equilibrium composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



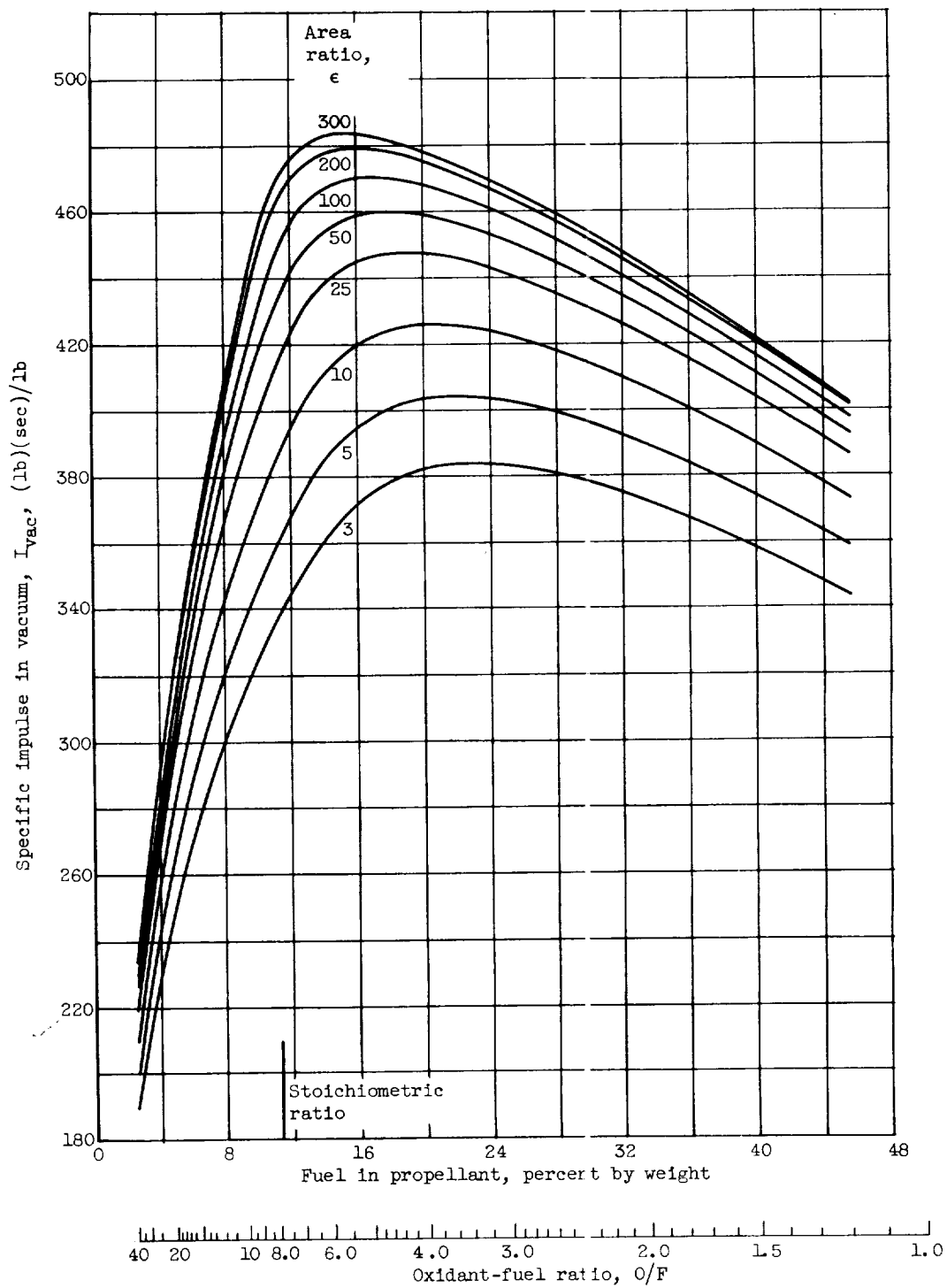
(a) Chamber pressure, 60 pounds per square inch absolute; frozen composition during expansion.

Figure 7. - Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



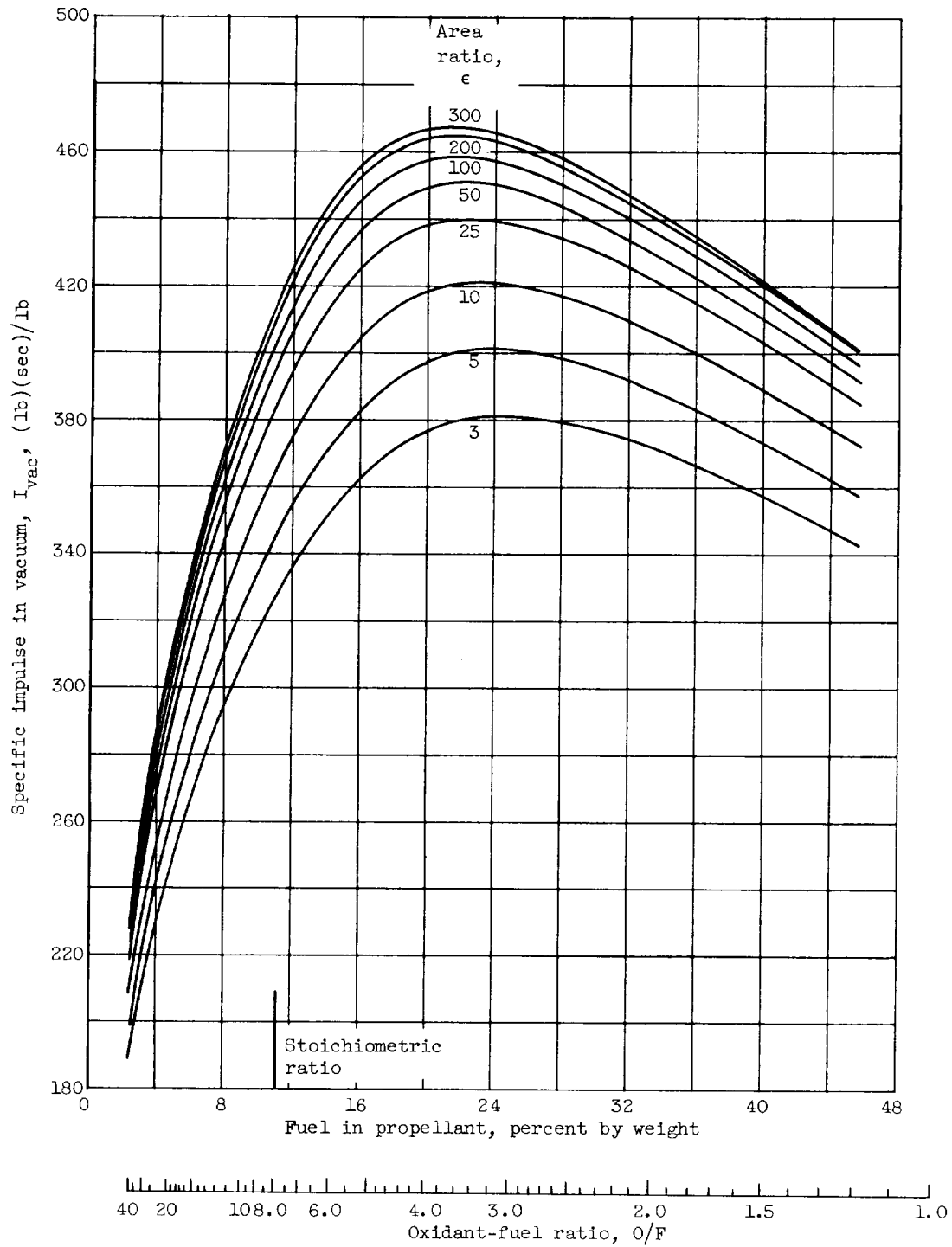
(c) Chamber pressure, 150 pounds per square inch absolute;
frozen composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



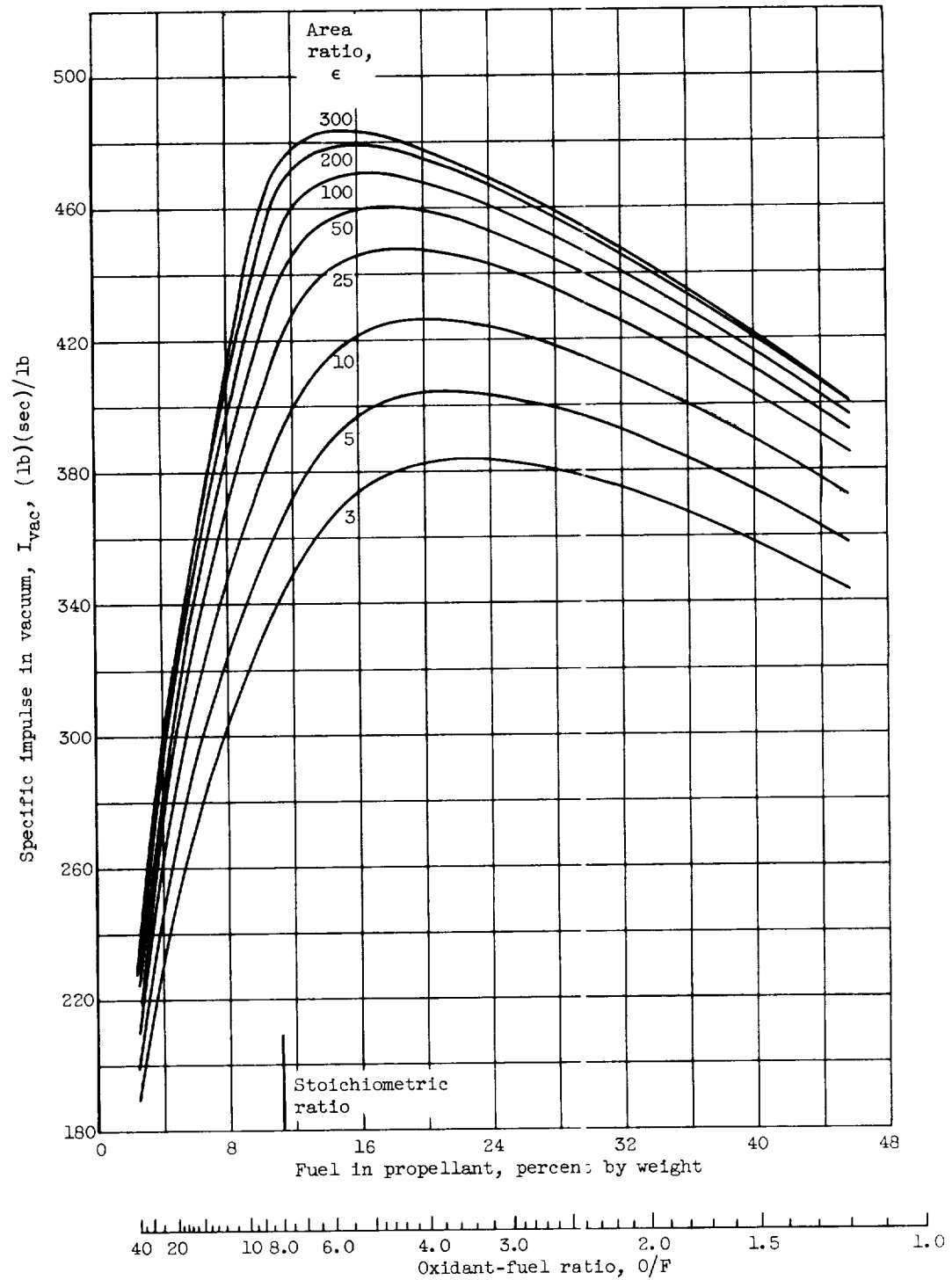
(d) Chamber pressure, 150 pounds per square inch absolute; equilibrium composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



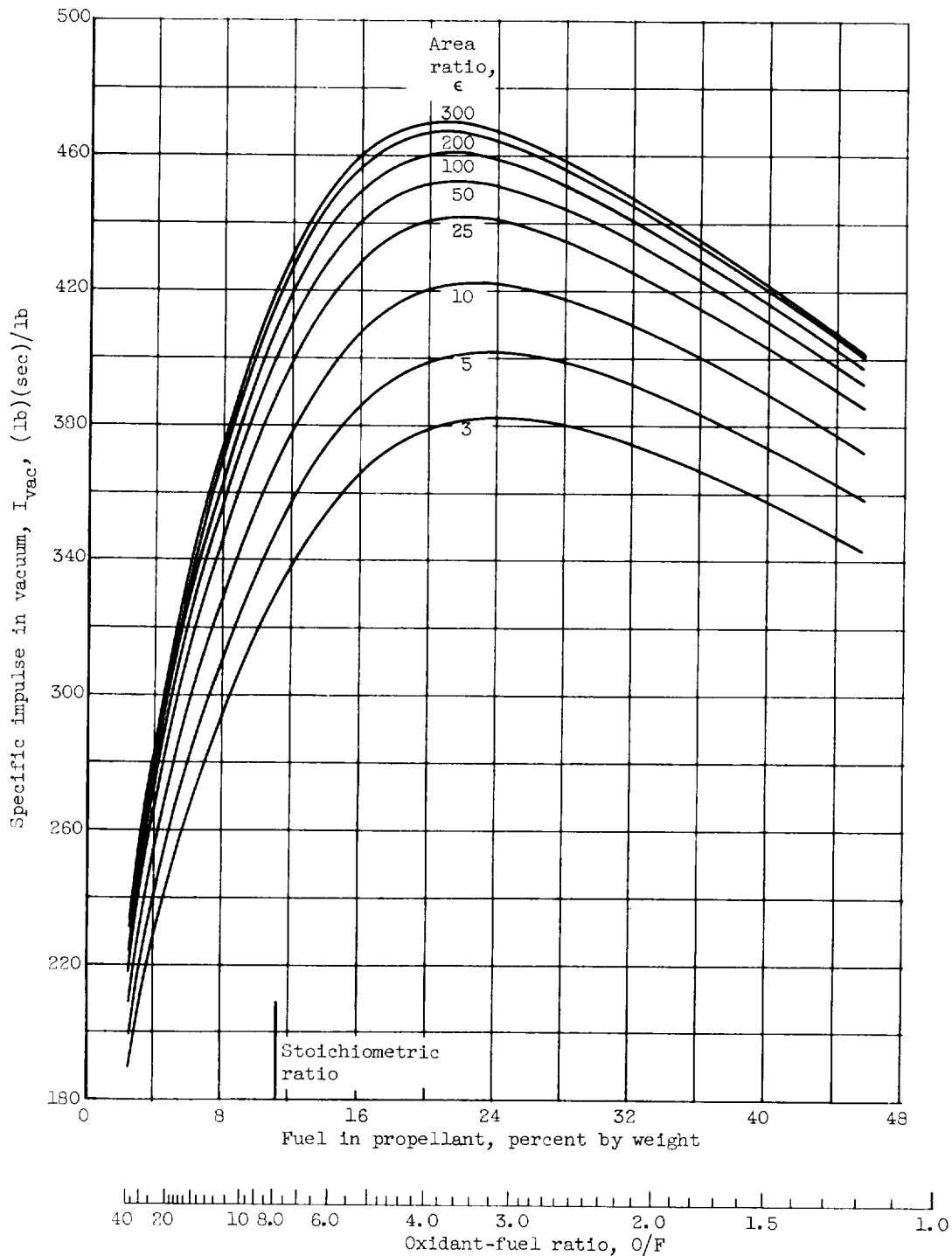
(e) Chamber pressure, 300 pounds per square inch absolute;
frozen composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



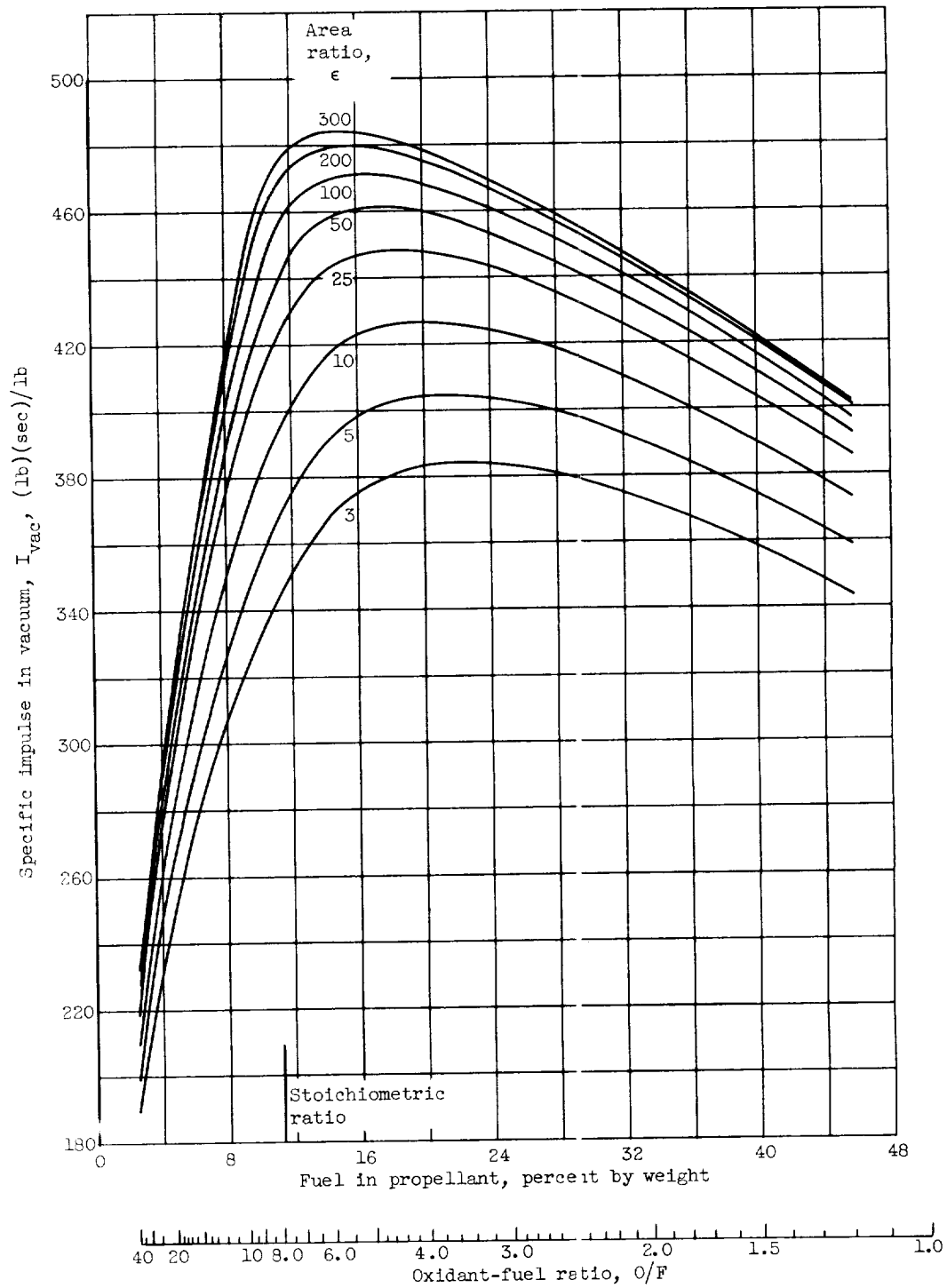
(f) Chamber pressure, 300 pounds per square inch absolute; equilibrium composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



(g) Chamber pressure, 600 pounds per square inch absolute;
frozen composition during expansion.

Figure 7. - Continued. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.



(h) Chamber pressure, 600 pounds per square inch absolute; equilibrium composition during expansion.

Figure 7. - Concluded. Theoretical specific impulse in vacuum of liquid hydrogen and liquid oxygen. Isentropic expansion to area ratio indicated.

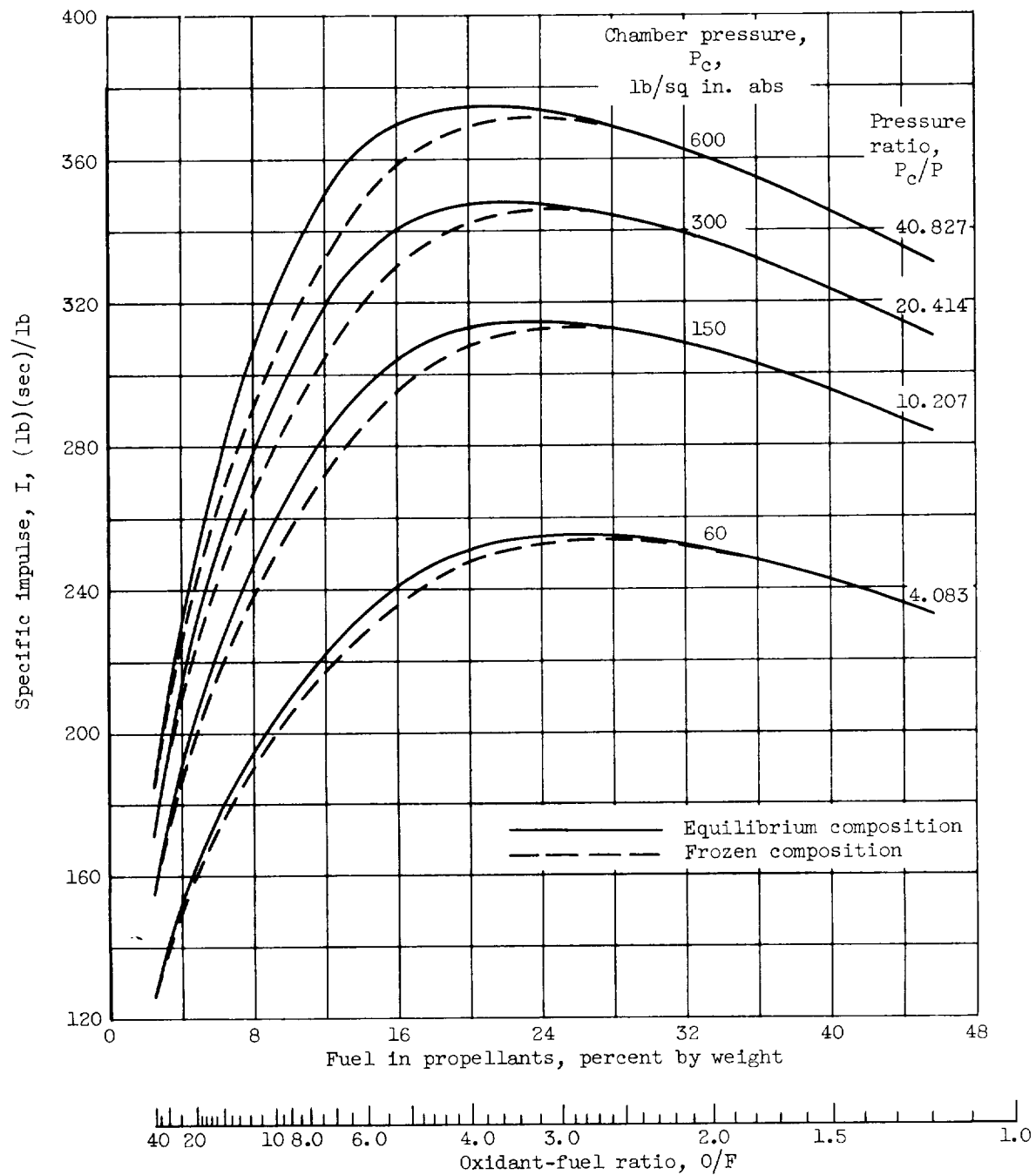


Figure 8. - Theoretical specific impulse for liquid hydrogen with liquid oxygen. Isentropic expansion to 1 atmosphere from chamber pressure indicated.

