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TWRS Privatization Process Technical Baseline

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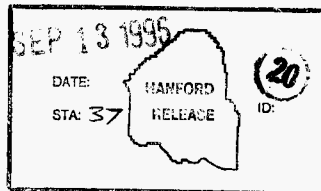
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Abstract: The U. S. Department of Energy (DOE) is planning a two-phased program for the remediation of Hanford tank waste. Phase 1 is a pilot program to demonstrate the procurement of treatment services. The volume of waste treated during Phase 1 is a small percentage of the tank waste. During Phase 2, DOE intends to procure treatment services for the balance of the waste. The *TWRS Privatization Process Technical Baseline* (PPTB) provides a summary level flowsheet/mass balance of tank waste treatment operations which is consistent with the tank inventory information, waste feed staging studies, and privatization guidelines currently available. The PPTB will be revised periodically as privatized processing concepts are crystallized.

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TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

TANK WASTE REMEDIATION SYSTEM PRIVATIZATION PROCESS TECHNICAL BASELINE

September 1996

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Prepared for
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WHC-SD-WM-TI-774 Rev. 0
TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

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SUMMARY

The operating contractor's¹ functions described in this *Privatization Process Technical Baseline (PPTB)* are supported by flowsheet work and substantial planning documentation developed previously for the Tank Waste Remediation System (TWRS). The private contractors' functions are modeled without any specific knowledge of their process technology, but within the limits and information currently available through the *TWRS Privatization Request for Proposals* (DOE-RL 1996). This situation will be remedied in future revisions of the *PPTB* when more information about the private contractors' processes becomes available. In the meantime, the reader is advised that the private contractor portion of the *PPTB* is tentative.

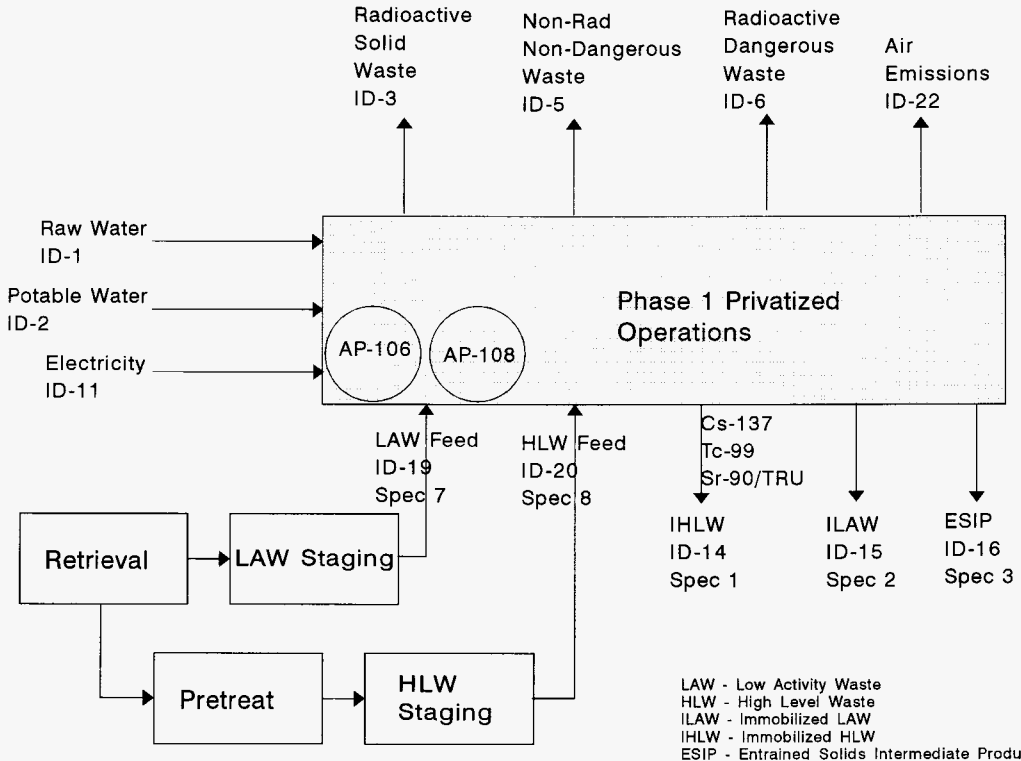
Phase 1

If the U.S. Department of Energy (DOE) elects to have one its Phase 1 private contractors immobilize high-level waste (HLW), then the Hanford operating contractor will pretreat selected HLW sludge. In any event, the operating contractor will prepare batches of supernate for further treatment by private contractors. For this *PPTB*, the DOE exercises the option to purchase immobilization services for pretreated HLW from one private contractor. DOE will likewise purchase services for the pretreatment of supernates and the immobilization of low-activity waste (LAW) from the HLW private contractor and from one other private contractor. Figure S-1 depicts the privatization concept for processing HLW and LAW. Figure S-2 depicts the privatization concept for processing LAW only. Throughout the *PPTB*, Private Contractor #1 (PC1) refers to the HLW private contractor; Private Contractor #2 (PC2) processes supernate only.

The operating contractor pretreats HLW sludges in AZ-101, AZ-102 and AY-102 (including retrieved C-106 sludge) and stages 375,000 kgs of washed sludges (oxide equivalent, not including Na and Si) in 16 batches to the HLW private contractor. Table S-1 summarizes the canister count of immobilized high-level waste (IHLW) returning from the HLW private contractor, assuming a standard canister size (1,650 kg or 0.62 m³) and a waste oxide loading of 25 wt% (not including Na, Si, or private contractor added material). Note that the HLW private contractor does not return separated strontium/transuranic (TRU), cesium, and technetium to the operating contractor as intermediate product, but incorporates this material with the IHLW product (see Figure S-1). Material balances for the pretreatment and immobilization of each tank are provided in Section 2.4. The mass of washed solids provided to PC1 is more than the minimum order of 245,000 kgs but less than the maximum order of 465,000 kgs. Additional feeds to meet the maximum order will be identified in future revisions.

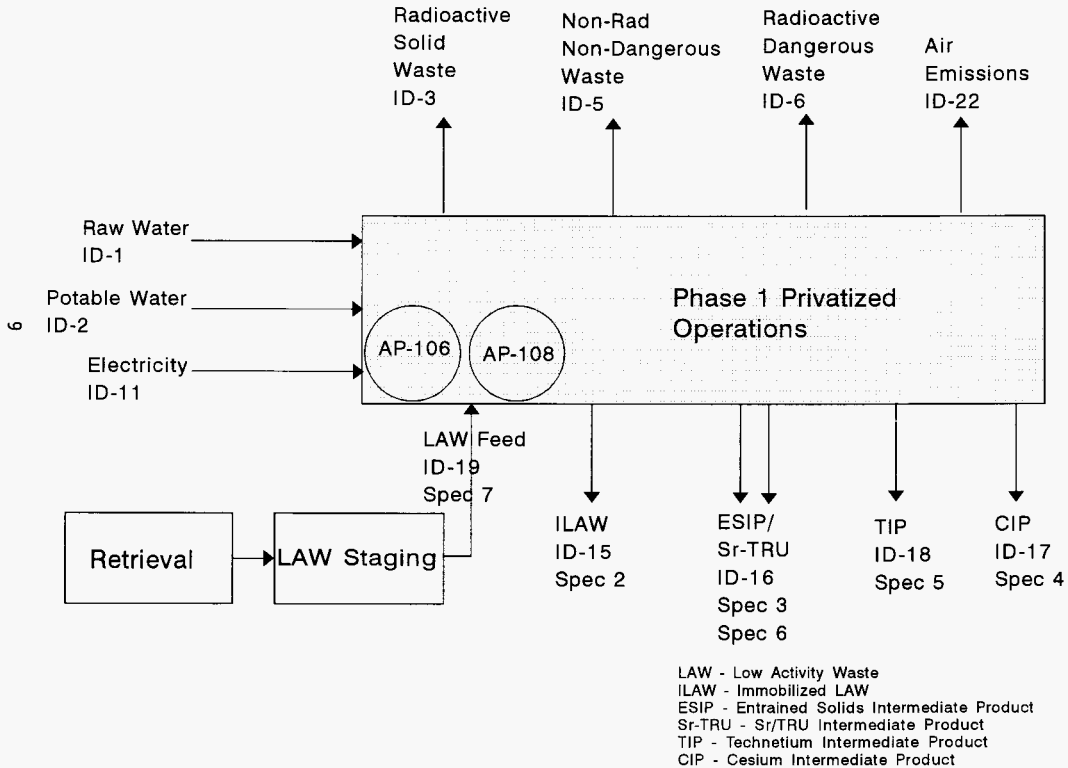
¹"Operating contractor" is a generic term having reference to the contractor(s) who conduct non-privatized operations for the DOE.

Figure S-1 HLW and LAW Processing



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Figure S-2 LAW Only Processing



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Twelve batches of supernate are prepared and staged to each of the private contractors. Each private contractor receives ~5,100 MT of soluble sodium for a total of ~10,200 MT of sodium. The private contractors separate solids and remove (as needed to satisfy DOE product specifications) strontium/TRU, cesium, and technetium. The pretreated LAW is immobilized in a currently unspecified waste form in 2.6 m³ ILAW packages. Table S-2 summarizes the radionuclide loading and ILAW package count for the 24 Phase 1 supernate batches. Appendix B provides material balances for each of the batches, including the volume of intermediate radionuclide products returned to the operating contractor.

Table S-1 Phase 1 IHLW Canister Count From PCI

Batch #	Canisters (1,650 kg or 0.62 m ³)
1(AZ-101)	94
2(AZ-101)	94
3(AZ-102)	81
4(AZ-102)	81
5(AY/C)	47
6(AY/C)	47
7(AY/C)	47
8(AY/C)	47
9(AY/C)	47
10(AY/C) ^a	47
11(AY/C)	47
12(AY/C)	47
13(AY/C)	46
14(AY/C)	46
15(AY/C)	46
16(AY/C)	46
Total	910

^aThis batch satisfies the HLW minimum order quantity.

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Table S-2 Phase 1 ILAW Product Summary and Package Count

Batch	Envelope		Private Contractor #1						Private Contractor #2							
			ILAW LOADING				ILAW	Cs ^b	ILAW LOADING				ILAW	Cs		
			TRU	Sr	Cs	Tc			TRU	Sr	Cs	Tc				
PC1	PC2	nCi/g	Ci/m ³	Ci/m ³	Ci/m ³	2.6m ³ Pkgs	Pkgs	nCi/g	Ci/m ³	Ci/m ³	Ci/m ³	2.6m ³ Pkgs	Pkgs			
1	A	A	6.1	4.5	3.0	0.18	708	4	6.3	4.5	3.0	0.18	683	4		
2	A	A	0.6	3.9	3.0	0.02	766	1	0.6	3.9	3.0	0.02	745	1		
3	A	A	6.0	13.3	3.0	0.17	497	4	6.0	13.3	3.0	0.17	496	4		
4	A	A	1.8	2.7	3.0	0.25	545	4	1.8	2.7	3.0	0.25	543	3		
5	A	A	2.0	14.5	3.0	0.20	733	5	2.0	14.5	3.0	0.20	733	5		
6	B	B	16.3	5.6	3.0	0.30	383	6	16.3	5.6	3.0	0.30	383	6		
7 ^a	C	C	100.0	20.0	3.0	0.30	147	1	100.0	20.0	3.0	0.30	147	1		
8 ^a	C	C	100.0	20.0	3.0	0.30	307	2	100.0	20.0	3.0	0.30	307	2		
9 ^a	C	C	96.1	20.0	3.0	0.30	605	2	96.5	20.0	3.0	0.30	601	2		
10	C	C	4.8	6.2	3.0	0.02	717	1	4.8	6.2	3.0	0.02	717	1		
11	C	C	2.5	20.0	3.0	0.05	714	1	4.9	20.0	3.0	0.10	704	1		
12	B	C	17.9	6.4	3.0	0.30	623	10	5.0	20.0	3.0	0.10	352	1		
							Total	6745	41					Total	6412	31

^aIn practice, the private contractors will target TRU concentration well below 100 nCi/g to ensure that ILAW is suitable for near-surface disposal.

^bShaded values are Cs packages not produced by HLW private contractor.

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Table S-2 shows the projected cesium intermediate product (CIP) package count for PC2. Table S-2 also indicates the number of cesium packages that are not produced by the HLW private contractor.

Phase 2

For Phase 2, DOE's intention is to continue procuring services from private contractors for the balance of the tank waste, expanding the scope to include all retrieval and pretreatment in addition to immobilization. There is nothing equivalent to the TWRS Privatization Request for Proposals (DOE-RL 1996) and feed staging plans (Manuel 1996, Certa 1996) to provide guidance for Phase 2. The feed to Phase 2 consists of all tank waste retrieved together into a composite feed stream, with adjustments to account for Phase 1 operations.

The PPTB models Phase 2 in a manner similar to previous TWRS Process Flowsheets (Orme 1994, Orme 1995). The composite feed is separated into sludge and supernates by a settle/decant operation. The sludges are subjected to caustic leaching to solubilize a portion of the solids, then washed to dilute the content of the interstitial liquid. The pretreated solids are then immobilized in glass. Enhanced sludge washing laboratory results indicate that chromium caustic leach is not very effective for certain wastes that were evaluated for the first time this year. Due to the large volume of these wastes, the net effect was a drastic reduction in the overall mass-weighted chromium caustic leach factor.

The PPTB projects a canister count of 22,420 standard canisters (1,650 kgs or 0.62 m^3 per canister) or 12,890 proposed standard canisters (2,870 kgs or 1.08 m^3 per canister) of IHLW from Phase 2.

The above results are based on the TWRS Inventory which was carried over from Revision 1 of the TWRS Process Flowsheet. The PPTB also considers a second inventory case which is based on draft standard inventory values (Kupfer et al. 1996). While the standard inventory is subject to change over the next year, these tentative values nonetheless indicate trends for certain key components. There will be a significant increase in the inventory of chromium. The current chromium solubility limit drives the canister count to 49,500 and 28,460 for the standard canister and proposed standard canister, respectively.

All liquid effluents from settle/decant separations are pretreated to remove cesium, thereby removing the primary soluble radionuclide, ^{137}Cs . Subsequent revisions of the PPTB will reflect additional separation requirements when and if they are added to Phase 2. The pretreated liquids are likewise immobilized in glass.

The past year's inventory and enhanced sludge washing developments focus future Phase 2 flowsheet efforts on controlling a burgeoning IHLW volume.

1.0 INTRODUCTION

Selected TWRS functions that are pertinent to the management and treatment of tank waste are depicted in Figure 1. Hanford's operating contractor will perform certain functions, but the DOE has elected to procure the services of private contractors for other functions. The DOE will pursue the privatization of waste treatment services in a two-phased approach. Figure 1 shows the current assignment of functions during the two phases of privatization. The TWRS PPTB is a summary-level flowsheet/mass balance of Phases 1 and 2.

During Phase 1, the Hanford operating contractor prepares and stages liquid wastes (supernates) to two private contractors that are providing LAW processing services. The operating contractor also pretreats and transfers HLW sludges from selected tanks to one of the two private contractors. These activities are categorized as LAW Staging Operations, and HLW Pretreatment and Staging Operations, respectively. The operating contractor ensures that waste is transferred to the private contractors on schedule and within contractual specifications. The private contractors receive waste transfers and treat the waste to contractual specifications, returning intermediate products and final products to the operating contractor for interim storage or disposal. Phase 1 is intended to be a demonstration, processing up to 13% of the water-soluble inventory and 6% of the HLW inventory.

Phase 2 private contractor requirements have not been finalized, although work to identify a Phase 2 retrieval and processing sequence is proceeding (Penwell 1996). For the purposes of the Phase 2 flowsheet/mass balance, the post-Phase 1 tank waste inventory is composited as a single feed stream and processed through a settle/decant-sludge washing-radionuclide separation-immobilization process similar (but not identical) to previous revisions of the TWRS Process Flowsheet (Orme 1995).

Table 1 compares some primary characteristics of the flowsheets for Phase 1 and Phase 2.


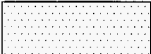
2.0 PHASE 1 FLOWSHEET/MASS BALANCE

Supernate preparation by the operating contractor generally consists of diluting double-shell tank (DST) supernates and batching appropriate amounts to the private contractors' receiving tanks. Both private contractors receive supernates, separate entrained solids, recover radionuclides (strontium/TRU, cesium, and technetium) from the supernates, convert them to intermediate products, and immobilize the decontaminated supernates.

The operating contractor conducts sludge-washing operations to prepare HLW sludges for PCI. PCI converts the sludges and intermediate radionuclide waste products recovered from supernates into an IHLW form in a container suitable for disposal at a geologic repository.

Figure 1 Privatization of TWRS Functions

Pre-Privatization	Phase 1 Assignments	Phase 2 Assignments
Store Managed Tank Waste	Store Managed Tank Waste	Store Managed Tank Waste
Characterize Waste	Characterize Waste	Characterize Waste
Transfer Managed Tank Waste	Transfer Managed Tank Waste	Transfer Managed Tank Waste
Concentrate Waste	Concentrate Waste	Concentrate Waste
Retrieve SSTs	Retrieve SSTs	Retrieve SSTs
Retrieve DSTs	Retrieve DSTs	Retrieve DSTs
Retrieve MUSTs	Retrieve MUSTs	Retrieve MUSTs
Store In-process Waste	Store In-process Waste	Store In-process Waste
Pretreat Sludges	Pretreat Sludges	Pretreat Sludges
Pretreat Supernatants	Pretreat Supernatants	Pretreat Supernatants
Immobilize LAW	Immobilize LAW	Immobilize LAW
Immobilize HLW	Immobilize HLW	Immobilize HLW

	Operating Contractor Functions		Privatized Functions
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Table 1 Comparison of Phase 1 and Phase 2 Flowsheets

	Phase 1	Phase 2
Number of Streams	Major streams only	Major streams only
Batching Approach	Batches from specific tanks conform to feed staging plans and comply with Phase 1 feed envelopes A, B, C and D	Composite the remainder of the waste as a single "batch"
Stream Composition	Same level of definition as Phase 2	Same level of definition as Phase 1
Inventory	Developed specifically for Phase 1 feed tanks	Existing global inventory from TWRS Process Flowsheet
Liquid/Solid Distribution	Developed specifically for Phase 1 feeds	Mass-weighted solubility factors based on available characterization and enhanced sludge-washing data
Process Technology for Sludges	Sludge washing (removal of interstitial liquid components by dilution)	Enhanced sludge washing (additional dilution of solids by caustic leaching and removal of interstitial components by dilution)
Process Technology for Supernates	Separation requirements only; no specific technology	Organic phase separation added to TWRS Process Flowsheet technology
Offgas Treatment	Not addressed (private contractor responsibility)	Included in TWRS Process Flowsheet model
Waste Loading in IHLW	25% (not including Na and Si)	Controlled by chromium
Sensitivity Cases	None	Revised TWRS inventory with selected standard inventory values

2.1 SUPERNATE STAGING OPERATIONS

Single-shell tank (SST) pumping and waste evaporation continue for several more years, so the inventory profile of DSTs is changing. Shelton (1996) has projected the supernate² content of DSTs into the Fiscal Year (FY)-2002 time frame.³ The projected supernate inventories are shown in Appendix A. As tank farm operations play out over the next few years, some of the actual transfers are likely to depart from Shelton's assumed transfers. Therefore, the DST feed batches described below will be revised one or more times before Phase 1 staging begins.

With Shelton's projected inventory as a starting point, Certa (1996) has developed a staging plan for selected Phase 1 supernates. Supernate staging operations revolve around two tanks (AP-102 and AP-104) set aside as operating contractor intermediate staging tanks, and two tanks (AP-106 and AP-108) that are turned over to the private contractors as LAW receiving tanks. For insight into logistical considerations and the rationale behind Phase 1 supernate feed selection, the reader is referred to the staging plan.

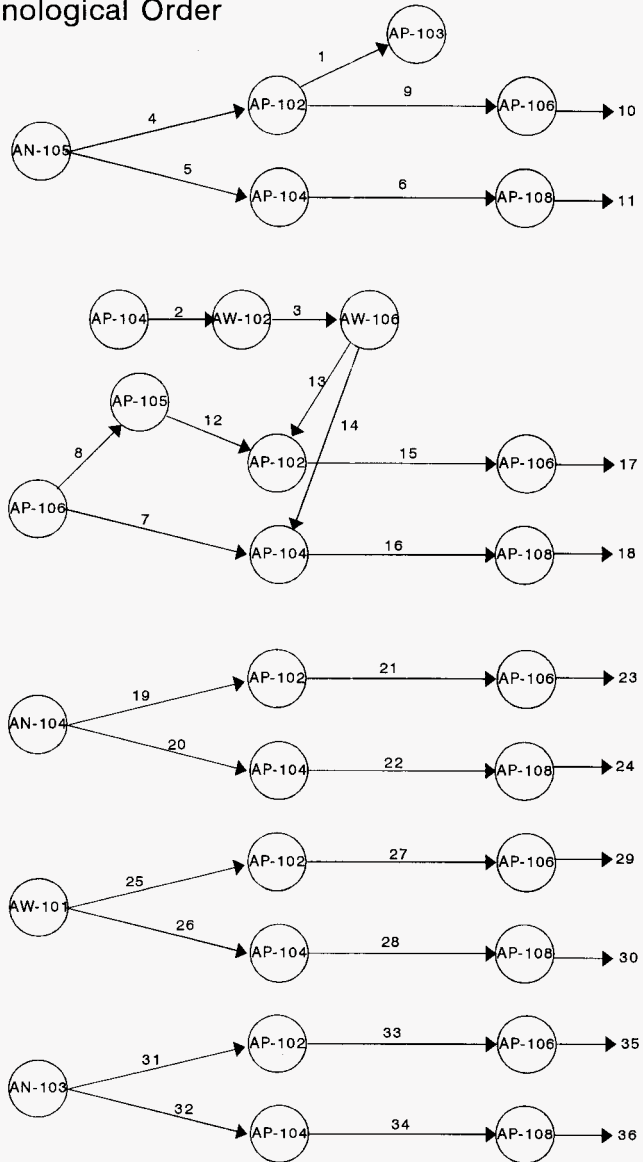
Figure 2 depicts the chronological order of the transfers that set up the supernate receiving tanks with the first 10 batches of Phase 1 Envelope A feed (each private contractor receives 5 batches). Several preliminary transfers are required to set up the initial batches of private contractor feed. For example, transfers #1 and #2 clear the existing waste out of AP-102 and AP-104, respectively, to prepare them for receiving Envelope A waste. Diagrams for Envelope B and C are not provided, but they would continue in a very similar pattern.

The operating contractor stages five batches of Envelope A, one batch of Envelope B, and one batch of Envelope C to each of two private contractors (PC1 and PC2) for the Phase 1 proof-of-concept (P-o-C). The Phase 1 extension provides four additional batches of Envelope C and one batch of Envelope B to PC1. PC2 receives five extension batches of Envelope C. Tables 2a and 2b summarize the batch inventory. These batches account for dilution by retrieval water, retrieval inefficiencies and heel mixing during the staging operations.

²The term "supernate" is used rather loosely in this context. Many DST supernates are highly concentrated, being close to or exceeding the solubility of some constituents. Precipitated salts are known to be present in some.

³Shelton's supernate projections are based on the near-term tank farm operating scenario outlined in Washenfelder (1996).

Figure 2 Diagram of Envelope "A" Staging Transfers in Chronological Order



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Table 2a PC1 LAW Feed Batches (2 sheets)

Batch	BATCH 1	BATCH 2	BATCH 3	BATCH 4	BATCH 5	BATCH 6	BATCH 7	BATCH 8	BATCH 9	BATCH 10	BATCH 11	BATCH 12
Date	01-Jun-02	03-Apr-03	17-Feb-04	16-Sep-04	04-May-05	06-Mar-06	05-Jun-06	13-Aug-06	25-Dec-06	09-Sep-07	06-Jul-08	30-Apr-09
Chemical	MT	MT	MT	MT	MT	MT	MT	MT	MT	MT	MT	MT
Al(OH)4-	3.43E+02	2.92E+02	1.94E+02	1.92E+02	3.56E+02	4.01E+01	6.09E+00	6.95E+00	9.18E+01	1.11E+02	1.10E+02	4.72E+01
Ba+2	2.89E-05	3.15E-04	1.46E-05	8.37E-07	3.93E-08	4.68E-05	5.03E-06	3.38E-06	3.83E-07	8.39E-05	1.39E-03	1.56E-04
Ca+2	7.30E-04	2.93E-02	1.36E-03	5.99E-02	1.51E-01	8.83E-03	2.65E-01	6.01E-01	8.41E-01	5.24E-02	5.29E-02	5.73E-03
Cd+2	1.39E-04	1.17E-04	5.37E-06	3.05E-07	2.71E-02	1.29E-03	1.21E-04	5.18E-05	5.52E-06	2.06E-04	1.96E-04	1.00E-05
Cr(OH)4-	3.26E+00	2.44E-01	2.15E+00	8.35E-01	3.37E+00	2.46E+00	4.51E-01	6.01E-01	1.22E+00	8.09E-02	4.23E-02	4.13E+00
Fe+3	2.31E-02	1.83E-02	1.61E-02	1.22E-03	1.19E-01	5.78E-03	7.22E-01	1.64E+00	1.98E-01	1.21E-02	4.39E-03	3.64E-04
Hg+2	0.00	3.47E-07	1.62E-08	9.24E-10	2.71E-02	1.29E-03	1.21E-04	5.18E-05	5.52E-06	7.22E-07	2.72E-07	1.35E-08
K+	1.27E+01	8.26E+00	1.02E+01	7.63E+01	3.11E+01	4.23E+00	1.45E+00	2.57E+00	7.12E+00	4.50E-01	1.58E+00	5.12E+00
La+3	0.00	1.89E-03	8.80E-05	5.03E-06	2.36E-07	4.99E-04	5.36E-05	3.61E-05	4.08E-06	1.89E-07	1.39E-02	1.61E-03
Na+	5.79E+02	6.27E+02	4.07E+02	4.46E+02	6.00E+02	1.26E+02	1.20E+02	2.51E+02	4.95E+02	5.87E+02	5.84E+02	2.04E+02
Ni+3	2.52E-03	2.15E-03	9.87E-05	5.61E-06	4.06E-02	2.45E-03	2.17E-01	4.91E-01	6.73E-01	4.18E-02	1.64E-02	1.73E-03
Pb+4	3.12E-04	7.45E-05	3.28E-06	5.47E-01	1.61E-01	7.22E-03	1.59E-01	3.60E-01	4.36E-02	3.01E-03	8.52E-04	4.20E-05
U	7.38E-04	1.69E-02	7.88E-04	4.05E-01	2.95E-02	8.86E-01	2.03E-01	3.09E-01	3.69E-02	2.06E-03	6.68E-03	1.59E+00
CO3-2	4.83E+01	8.26E+01	4.26E+01	2.54E+01	1.69E+01	3.76E+01	4.01E+01	8.45E+01	1.27E+02	9.60E+01	9.42E+01	7.08E+01
Cl-	1.81E+01	2.93E+01	1.17E+01	1.02E+01	1.70E+01	9.26E-01	1.58E+00	3.42E+00	7.21E+00	4.75E-01	2.43E-01	2.35E-01
F-	7.58E-01	2.64E+01	1.23E+00	7.03E-02	1.25E+00	1.74E+00	1.86E-01	1.24E-01	3.65E+00	4.66E+00	4.63E+00	3.25E+00
SO4-2	1.40E+01	1.73E+01	9.78E+00	2.59E+00	2.88E+00	2.08E+01	8.82E+00	1.64E+01	2.71E+01	1.88E+01	1.88E+01	3.81E+01
NO3-	4.07E+02	4.85E+02	2.86E+02	4.08E+02	2.99E+02	7.41E+01	1.22E+02	2.63E+02	4.17E+02	4.51E+02	4.49E+02	1.31E+02
NO2-	2.50E+02	2.33E+02	1.32E+02	1.94E+02	2.47E+02	6.71E+01	3.07E+01	5.83E+01	1.53E+02	1.86E+02	1.83E+02	1.09E+02
PO4-3	5.21E+00	1.27E+01	4.42E+00	4.14E+00	1.86E+00	1.01E+00	3.62E-01	6.48E-01	8.68E+00	1.17E+01	1.15E+01	2.24E+00
OH-	1.29E+02	1.46E+02	1.02E+02	1.64E+02	1.77E+02	1.74E+01	1.03E+01	2.05E+01	2.12E+01	1.64E+01	1.93E+01	1.72E+01
TOC	8.44E+00	1.82E+01	7.16E+00	4.97E+00	1.28E+01	2.27E+00	2.09E+01	4.70E+01	5.15E+01	8.36E+01	8.29E+01	7.20E+00

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Table 2a PC1 LAW Feed Batches (2 sheets)

Batch	BATCH 1	BATCH 2	BATCH 3	BATCH 4	BATCH 5	BATCH 6	BATCH 7	BATCH 8	BATCH 9	BATCH 10	BATCH 11	BATCH 12
Nuclide	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci
14C	4.73E-02	6.55E-03	2.76E-04	6.66E-01	3.43E+00	1.89E+00	2.01E-01	1.31E-01	3.19E+01	2.03E+00	9.16E-02	3.10E+00
90Sr	6.61E+03	6.26E+03	1.38E+04	3.02E+03	2.22E+04	4.46E+03	4.48E+04	1.01E+05	1.50E+05	9.32E+03	4.39E+04	8.37E+03
90Y	6.61E+03	6.26E+03	1.38E+04	3.02E+03	2.22E+04	4.46E+03	4.48E+04	1.01E+05	1.50E+05	9.32E+03	4.39E+04	8.37E+03
99Tc	2.71E+02	2.48E+01	1.81E+02	2.86E+02	3.08E+02	3.55E+02	1.87E+02	3.64E+02	5.84E+02	3.66E+01	7.23E+01	6.15E+02
137Cs	1.03E+06	6.12E+04	1.04E+06	9.62E+05	1.34E+06	1.77E+06	3.14E+05	4.09E+05	4.97E+05	3.12E+04	4.10E+04	3.06E+06
137Ba	9.80E+05	5.82E+04	9.86E+05	9.14E+05	1.27E+06	1.68E+06	2.98E+05	3.89E+05	4.72E+05	2.96E+04	3.89E+04	2.90E+06
154Eu	0.00	2.10E-04	9.77E-06	5.58E-07	2.62E-08	2.69E+03	2.89E+02	1.95E+02	1.41E+03	8.92E+01	3.56E+00	4.83E+03
235U	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
238U	1.12E-04	2.01E-04	9.32E-06	1.36E-01	9.90E-03	2.98E-01	6.83E-02	1.04E-01	1.24E-02	5.86E-04	1.46E-03	5.33E-01
237Np	1.53E-04	4.45E-03	2.07E-04	1.18E-05	3.39E-02	7.44E-02	7.97E-03	5.32E-03	6.02E-04	2.78E-05	9.76E-07	1.30E-01
238Pu	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
239Pu	1.67E+01	1.19E+00	1.14E+01	2.54E+00	3.38E+00	1.26E+01	1.44E+01	3.05E+01	1.06E+02	6.69E+00	2.38E+00	2.23E+01
240Pu	4.17E+00	2.98E-01	2.86E+00	6.34E-01	8.45E-01	3.14E+00	3.59E+00	7.62E+00	2.66E+01	1.67E+00	5.95E-01	5.58E+00
241Pu	2.63E+01	1.88E+00	1.80E+01	4.00E+00	5.33E+00	1.98E+01	2.26E+01	4.80E+01	1.67E+02	1.05E+01	3.74E+00	3.52E+01
241Am	3.07E+00	1.07E+00	2.12E+00	2.33E+00	4.06E+00	1.91E+01	3.03E+02	6.84E+02	1.91E+02	1.08E+01	7.03E+00	3.42E+01
Vol (L)	3.62E+06	4.10E+06	2.53E+06	2.77E+06	3.73E+06	1.11E+06	7.81E+05	1.58E+06	3.07E+06	3.65E+06	3.63E+06	1.86E+06
Na (M)	6.95E+00	6.65E+00	6.99E+00	6.99E+00	6.99E+00	4.92E+00	6.69E+00	6.91E+00	7.01E+00	6.99E+00	6.99E+00	4.77E+00
SpG	1.33E+00	1.31E+00	1.31E+00	1.37E+00	1.32E+00	1.23E+00	1.26E+00	1.27E+00	1.28E+00	1.27E+00	1.27E+00	1.22E+00

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Table 2b PC2 LAW Feed Batches (2 sheets)

Batch	BATCH 1	BATCH 2	BATCH 3	BATCH 4	BATCH 5	BATCH 6	BATCH 7	BATCH 8	BATCH 9	BATCH 10	BATCH 11	BATCH 12
Date	01-Jun-02	14-Mar-03	19-Jan-04	18-Aug-04	04-Apr-05	04-Feb-06	05-May-06	14-Jul-06	25-Nov-06	10-Aug-07	06-Jun-08	27-Mar-09
Chemical	MT	MT	MT	MT	MT	MT	MT	MT	MT	MT	MT	MT
Al(OH) ₃	3.34E+02	2.92E+02	1.94E+02	1.91E+02	3.56E+02	4.01E+01	6.09E+00	6.95E+00	9.12E+01	1.11E+02	1.08E+02	5.39E+01
Ba ²⁺	1.58E-05	3.09E-04	1.44E-05	8.25E-07	3.89E-08	4.68E-05	5.03E-06	3.38E-06	3.82E-07	8.39E-05	2.69E-03	1.41E-03
Ca ²⁺	6.55E-05	2.96E-02	1.38E-03	5.96E-02	1.51E-01	8.83E-03	2.65E-01	6.01E-01	8.35E-01	5.24E-02	1.03E-01	5.34E-02
Cd ²⁺	5.73E-04	1.25E-04	5.46E-06	3.05E-07	2.71E-02	1.29E-03	1.21E-04	5.18E-05	5.52E-06	2.06E-04	1.74E-04	8.62E-05
Cr(OH) ₃	3.13E+00	2.38E-01	2.15E+00	8.32E-01	3.37E+00	2.46E+00	4.51E-01	6.01E-01	1.21E+00	8.09E-02	7.66E-02	3.87E-02
Fe ³⁺	2.33E-02	1.85E-02	1.62E-02	1.22E-03	1.19E-01	5.78E-03	7.22E-01	1.64E+00	1.98E-01	1.21E-02	5.62E-03	2.72E-03
Hg ²⁺	0.00	3.47E-07	1.62E-08	9.26E-10	2.71E-02	1.29E-03	1.21E-04	5.18E-05	5.52E-06	7.23E-07	3.39E-08	1.27E-09
K ⁺	1.24E+01	8.45E+00	1.02E+01	7.60E+01	3.11E+01	4.23E+00	1.45E+00	2.57E+00	7.07E+00	4.50E-01	3.14E+00	1.64E+00
La ³⁺	0.00	1.83E-03	8.52E-05	4.87E-06	2.29E-07	4.99E-04	5.36E-05	3.61E-05	4.08E-06	1.90E-07	2.78E-02	1.46E-02
Na ⁺	5.59E+02	6.09E+02	4.06E+02	4.44E+02	6.00E+02	1.26E+02	1.20E+02	2.51E+02	4.91E+02	5.87E+02	5.76E+02	2.88E+02
Ni ³⁺	3.95E-05	1.95E-03	9.11E-05	5.20E-06	4.06E-02	2.45E-03	2.17E-01	4.91E-01	6.68E-01	4.18E-02	3.10E-02	1.55E-02
Pb ²⁺	1.06E-13	5.66E-05	2.64E-06	5.45E-01	1.61E-01	7.22E-03	1.59E-01	3.60E-01	4.36E-02	3.02E-03	6.37E-04	2.74E-04
U	5.76E-04	1.72E-02	8.04E-04	4.03E-01	2.94E-02	8.86E-01	2.03E-01	3.09E-01	3.69E-02	2.07E-03	1.30E-02	6.78E-03
CO ₃ ²⁻	4.46E+01	7.94E+01	4.25E+01	2.53E+01	1.69E+01	3.76E+01	4.01E+01	8.45E+01	1.26E+02	9.60E+01	9.47E+01	4.74E+01
Cl ⁻	1.73E+01	2.99E+01	1.17E+01	1.02E+01	1.70E+01	9.26E-01	1.58E+00	3.42E+00	7.16E+00	4.75E-01	4.41E-01	2.23E-01
F ⁻	2.23E-01	2.68E+01	1.25E+00	7.15E-02	1.25E+00	1.74E+00	1.86E-01	1.24E-01	3.63E+00	4.66E+00	4.55E+00	2.28E+00
SO ₄ ²⁻	1.33E+01	1.67E+01	9.75E+00	2.58E+00	2.88E+00	2.08E+01	8.82E+00	1.64E+01	2.69E+01	1.88E+01	1.94E+01	9.73E+00
NO ₃ ⁻	3.92E+02	4.71E+02	2.85E+02	4.06E+02	2.99E+02	7.41E+01	1.22E+02	2.63E+02	4.15E+02	4.51E+02	4.47E+02	2.23E+02
NO ₂ ⁻	2.43E+02	2.28E+02	1.32E+02	1.93E+02	2.47E+02	6.71E+01	3.07E+01	5.83E+01	1.52E+02	1.86E+02	1.79E+02	8.95E+01
PO ₄ ³⁻	3.97E+00	1.23E+01	4.40E+00	4.12E+00	1.86E+00	1.01E+00	3.62E-01	6.48E-01	6.82E+00	1.17E+01	1.12E+01	5.57E+00
OH ⁻	1.26E+02	1.48E+02	1.02E+02	1.63E+02	1.77E+02	1.74E+01	1.03E+01	2.05E+01	2.10E+01	1.64E+01	2.26E+01	1.15E+01
TOC	7.97E+00	1.41E+01	6.97E+00	4.95E+00	1.28E+01	2.27E+00	2.09E+01	4.70E+01	5.12E+01	8.36E+01	8.03E+01	4.01E+01

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Table 2b PC2 LAW Feed Batches (2 sheets)

Batch	BATCH 1	BATCH 2	BATCH 3	BATCH 4	BATCH 5	BATCH 6	BATCH 7	BATCH 8	BATCH 9	BATCH 10	BATCH 11	BATCH 12
Nuclide	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci	Ci
14C	7.51E-10	3.96E-03	1.85E-04	6.63E-01	3.43E+00	1.89E+00	2.01E-01	1.31E-01	3.17E+01	2.03E+00	1.01E-01	1.34E-02
90Sr	6.48E+03	6.05E+03	1.38E+04	3.01E+03	2.22E+04	4.46E+03	4.48E+04	1.01E+05	1.49E+05	9.32E+03	8.74E+04	4.58E+04
90Y	6.48E+03	6.05E+03	1.38E+04	3.01E+03	2.22E+04	4.46E+03	4.48E+04	1.01E+05	1.49E+05	9.32E+03	8.74E+04	4.58E+04
99Tc	2.63E+02	2.40E+01	1.80E+02	2.85E+02	3.08E+02	3.55E+02	1.87E+02	3.64E+02	5.80E+02	3.66E+01	1.43E+02	7.45E+01
137Cs	1.01E+06	5.99E+04	1.04E+06	9.59E+05	1.34E+06	1.77E+06	3.14E+05	4.09E+05	4.94E+05	3.12E+04	8.03E+04	4.16E+04
137Ba	9.60E+05	5.69E+04	9.86E+05	9.11E+05	1.27E+06	1.68E+06	2.98E+05	3.89E+05	4.69E+05	2.96E+04	7.63E+04	3.96E+04
154Eu	0.00	2.10E-04	9.79E-06	5.60E-07	2.64E-08	2.69E+03	2.89E+02	1.95E+02	1.40E+03	8.91E+01	3.56E+00	1.25E-01
235U	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
238U	4.18E-06	1.89E-04	8.82E-06	1.35E-01	9.89E-03	2.98E-01	6.83E-02	1.04E-01	1.24E-02	5.89E-04	2.90E-03	1.52E-03
237Np	5.31E-08	4.58E-03	2.14E-04	1.22E-05	3.39E-02	7.44E-02	7.97E-03	5.32E-03	6.01E-04	2.80E-05	9.82E-07	3.20E-08
238Pu	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
239Pu	1.67E+01	1.18E+00	1.14E+01	2.53E+00	3.38E+00	1.26E+01	1.44E+01	3.05E+01	1.06E+02	6.69E+00	4.49E+00	2.23E+00
240Pu	4.17E+00	2.96E-01	2.86E+00	6.33E-01	8.45E-01	3.14E+00	3.59E+00	7.62E+00	2.64E+01	1.67E+00	1.12E+00	5.57E-01
241Pu	2.63E+01	1.86E+00	1.80E+01	3.99E+00	5.33E+00	1.98E+01	2.26E+01	4.80E+01	1.66E+02	1.05E+01	7.06E+00	3.51E+00
241Am	3.03E+00	1.04E+00	2.12E+00	2.32E+00	4.06E+00	1.91E+01	3.03E+02	6.84E+02	1.90E+02	1.08E+01	1.36E+01	6.97E+00
Vol (L)	3.62E+06	4.09E+06	2.53E+06	2.76E+06	3.73E+06	1.11E+06	7.81E+05	1.58E+06	3.05E+06	3.65E+06	3.58E+06	1.79E+06
Na (M)	6.71E+00	6.47E+00	6.98E+00	6.99E+00	6.99E+00	4.92E+00	6.69E+00	6.91E+00	7.01E+00	6.99E+00	7.00E+00	7.00E+00
SpG	1.32E+00	1.31E+00	1.31E+00	1.37E+00	1.32E+00	1.23E+00	1.26E+00	1.27E+00	1.28E+00	1.27E+00	1.27E+00	1.27E+00

2.1.1 Chemistry of Phase 1 Envelope A

The following sections discuss the chemical and phase equilibrium of Envelope A feeds during dilution, as modeled with the Environmental Simulation Program (ESP). There are known deficiencies with the ESP software, so it is not fully validated, but for the most part ESP predictions are qualitatively (if not quantitatively) consistent with experimental observation. The known deficiencies are discussed below, where appropriate.⁴

Envelope A tanks typically contain non-complexed waste with sodium ranging from 10 to 15 mol/L. Concentrated solutions containing aluminum can exhibit unexpected precipitation when diluted. The solubility of aluminum is a complex function of hydroxide, as well as total ionic strength. The main purpose of this modeling was to identify tanks that have the potential to be problematical. The tanks are discussed below in the order of staging.

2.1.1.1 AN-105 Staging

The following simulation results suggest that further modeling studies and experimental work with actual AN-105 supernate are warranted to verify suitable conditions for its recovery and staging.

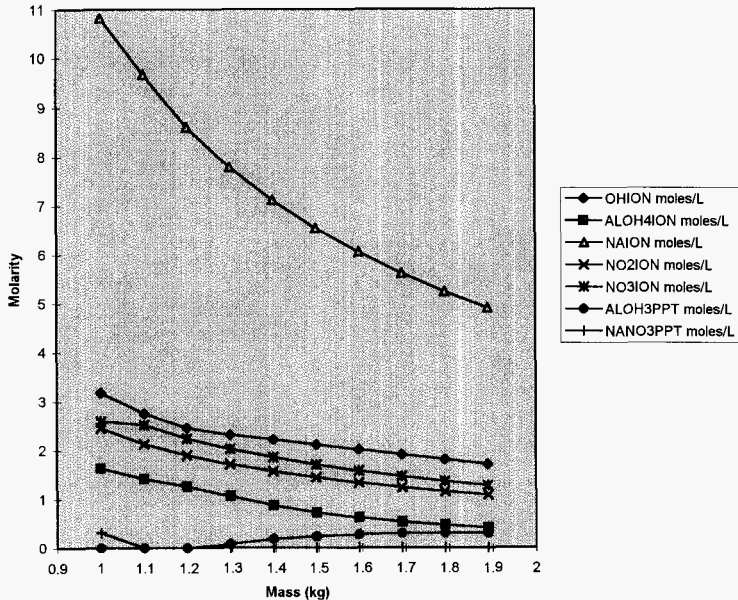
The chemical and phase equilibrium of AN-105 supernate at 40 °C was modeled with the ESP. Table 3 and Figure 3 depict the phase equilibrium for a unit mass of AN-105 supernate as it is diluted with water. The presence of NaNO_3 precipitate indicates that this supernate is saturated at this temperature, so pipeline transfer without heating or dilution is not advisable. Dilution with water down to approximately 9.5M Na dissolves the salts. Dilution beyond 8.5M Na favors the precipitation of gibbsite ($\text{Al}(\text{OH})_3$). Continuing the dilution down to 7M Na, the concentration assumed for the staging plan (Certa 1996), generates approximately 0.14 kg gibbsite per kg diluted supernate (0.2 kg gibbsite per kg of supernate). Such extensive precipitation would exceed the allowable 5 vol% settled solids in feeds transferred to the private contractors.

⁴ESP is a trademark of OLI Systems, Inc. ESP results provide insight into the chemistry of high ionic strength mixtures, but experimental verification is advisable. For a discussion of how the ESP electrolyte simulation was used to support this work, refer to Appendix C.

Table 3 AN-105 Dilution @ 40 C

Mass kgs	OHION moles/L	ALOH4ION moles/L	NAION moles/L	NO2ION moles/L	NO3ION moles/L	ALOH3PPT moles/L	NANO3PPT moles/L
1.000	3.180	1.635	10.823	2.450	2.600	0.000	0.309
1.099	2.761	1.420	9.668	2.128	2.519	0.000	0.000
1.198	2.460	1.265	8.605	1.896	2.241	0.000	0.000
1.297	2.310	1.062	7.788	1.716	2.028	0.082	0.000
1.395	2.218	0.866	7.117	1.568	1.853	0.180	0.000
1.494	2.112	0.723	6.542	1.442	1.703	0.239	0.000
1.593	2.006	0.616	6.050	1.333	1.575	0.273	0.000
1.692	1.903	0.534	5.620	1.239	1.464	0.292	0.000
1.791	1.806	0.469	5.246	1.156	1.366	0.302	0.000
1.890	1.715	0.417	4.917	1.084	1.281	0.306	0.000

Figure 3 AN-105 Dilution @ 40 C



For the time, being the flowsheet acknowledges precipitation as a potential problem, but does not propose control measures.⁵ Subsequent dilution by private contractors could precipitate more gibbsite.

The retrieval of AN-105 supernate requires mixer pumps and in-line dilution to generate a stream that is suitable for pipeline transfer.

2.1.1.2 AP-104 Staging

AP-104 contains a dilute supernate that is evaporated during staging. The concentrate, residing in AW-106, tops off the next two batches of feed that originate from AP-106 (See Section 2.1.1.3, "AP-106 Staging").

2.1.1.3 AP-106 Staging

Figure 2 depicts the chronological order of a series of transfers whose net effect is to set up the LAW receiving tanks with their second batch of private contractor feed. AP-106 is diluted and split between the two operating contractor staging tanks. Half of AP-106 is retrieved directly into a staging tank (AP-104). The other half reaches AP-102 via AP-105.

Not being quite as concentrated as AN-105, AP-106 is mobilized with a recirculation loop and equipped with in-line dilution to generate a stream that is suitable for pipeline transfer.

The phase equilibrium and chemistry of AP-106 supernate during dilution at 40 °C was modeled with the ESP. Table 4 and Figure 4 depict the phase equilibrium for a unit mass of AP-106 supernate. The high fluoride content is illustrated by the presence of NaF precipitate. Cooling this supernate to 25 °C also precipitates gibbsite, so pipeline transfer without heating or dilution is not advisable. Dilution down to $\sim 9M$ Na generates gibbsite, with a large amount of gibbsite appearing for dilutions to $7M$ Na, the concentration assumed for the staging plan (Certa 1996). The private contractors should be aware that further dilution could cause precipitation. (Note: The ESP calculated initial concentration of hydroxide is somewhat lower than expected, although the other species appear to be correct. This may contribute to the early onset of gibbsite formation in this model run, since higher hydroxide helps to keep the aluminum in solution).

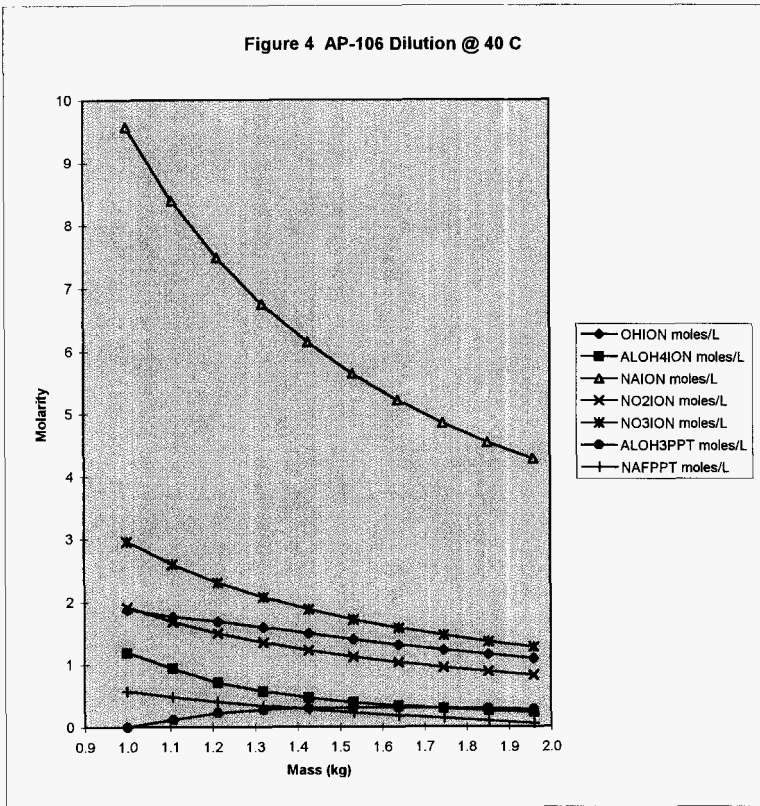
⁵Measures to deal with precipitation will be addressed in future revisions of the staging plan and the PPTB. Prevention by chemical adjustment is one option for dealing with precipitates. If the precipitation is minor, physical separation in the staging tanks could be a preferable alternative. Either approach will change the composition of the private contractor feed, which must remain within the contractual feed composition window.

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Table 4 AP-106 Dilution @ 40 C

Mass kgs	OHION moles/L	ALOH4ION moles/L	NAION moles/L	NO2ION moles/L	NO3ION moles/L	ALOH3PPT moles/L	NAFPPT moles/L
1.000	1.876	1.191	9.570	1.917	2.962	0.000	0.569
1.107	1.761	0.928	8.398	1.681	2.593	0.117	0.478
1.213	1.685	0.706	7.489	1.495	2.306	0.223	0.402
1.320	1.588	0.561	6.749	1.343	2.071	0.273	0.335
1.427	1.487	0.461	6.143	1.218	1.878	0.296	0.276
1.533	1.391	0.388	5.637	1.112	1.715	0.303	0.223
1.640	1.304	0.333	5.213	1.023	1.578	0.302	0.176
1.746	1.224	0.291	4.853	0.947	1.461	0.297	0.133
1.853	1.152	0.258	4.544	0.881	1.359	0.290	0.093
1.960	1.087	0.231	4.277	0.824	1.271	0.281	0.056

Figure 4 AP-106 Dilution @ 40 C



2.1.1.4 AN-104 Staging

The phase equilibrium and chemistry of AN-104 supernate during dilution at 40 °C was modeled with the ESP. Table 5 and Figure 5 depict the phase equilibrium for a unit mass of AN-104 supernate. The presence of NaNO_2 precipitate indicates that this supernate is saturated at this temperature, so pipeline transfer without heating or dilution is not advisable. Dilution down to 6M Na generates gibbsite, but no gibbsite appears for dilutions to 7M Na, the concentration assumed for the staging plan (Certa 1996). Subsequent dilution by private contractors could cause precipitation.

2.1.1.5 AW-101 Staging

The phase equilibrium and chemistry of AW-101 supernate during dilution at 40 °C was modeled with ESP. Table 6 and Figure 6 depict the phase equilibrium for a unit mass of AW-101 supernate. The presence of KNO_3 precipitate indicates that this supernate is saturated at this temperature, so pipeline transfer without heating or dilution is not advisable. Dilution beyond 5M Na begins to generate gibbsite, but no gibbsite appears for dilutions to 7M Na, the concentration assumed for the staging plan (Certa 1996). Subsequent dilution by private contractors could cause precipitation.

2.1.1.6 AN-103 Staging

The phase equilibrium and chemistry of AN-103 supernate during dilution at 40 °C was modeled with ESP. Table 7 and Figure 7 depict the phase equilibrium for a unit mass of AN-103 supernate. The presence of large amounts of precipitated salt is consistent with this tank's designation as a Double-Shell Slurry (DSS) tank. Pipeline transfer without heating or dilution is not advisable. Dilution down to 7M Na, the concentration assumed for the staging plan (Certa 1996), appears to be possible without gibbsite formation, but gibbsite precipitates at a slightly lower sodium concentration. Subsequent dilution by private contractors could cause precipitation.

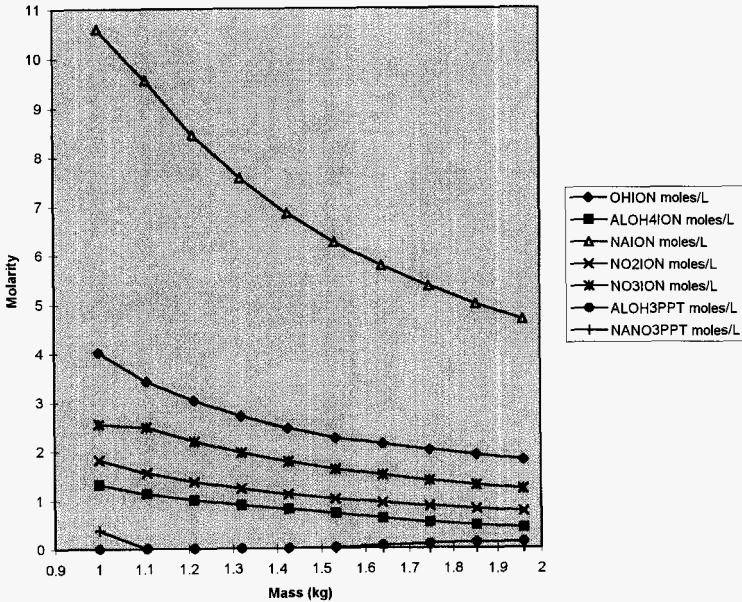
DSS was concentrated beyond the phase boundary where NaAlO_2 should have formed. A known deficiency of the current version of ESP is that it does not predict the existence of NaAlO_2 precipitate when that compound should obviously be present. The ESP data banks are being corrected to fix this deficiency, but the fix will not be available in time to include in this release. The equilibrium at the dilute end of Figure 7, however, should be valid.

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Table 5 AN-104 Dilution @ 40C

Mass kgs	OHION moles/L	ALOH4ION moles/L	NAION moles/L	NO2ION moles/L	NO3ION moles/L	ALOH3PPT moles/L	NANO3PPT moles/L
1.000	4.015	1.320	10.590	1.822	2.547	0.000	0.375
1.107	3.420	1.124	9.552	1.552	2.483	0.000	0.000
1.213	3.024	0.994	8.443	1.373	2.194	0.000	0.000
1.320	2.711	0.891	7.564	1.230	1.964	0.000	0.000
1.427	2.454	0.806	6.844	1.113	1.777	0.000	0.000
1.534	2.257	0.722	6.255	1.017	1.624	0.014	0.000
1.640	2.133	0.615	5.768	0.938	1.497	0.064	0.000
1.747	2.016	0.533	5.348	0.870	1.389	0.097	0.000
1.854	1.907	0.468	4.983	0.810	1.294	0.119	0.000
1.960	1.806	0.416	4.663	0.758	1.211	0.133	0.000

Figure 5 AN-104 Dilution @ 40 C



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Table 6 AW-101 Dilution @ 40 C

Mass kgs	OHION moles/L	ALOH4ION moles/L	NAION moles/L	NO2ION moles/L	NO3ION moles/L	ALOH3PPT moles/L	KNO3PPT moles/L
1.000	3.392	0.964	9.227	2.067	3.139	0.000	0.051
1.112	2.932	0.833	7.969	1.786	2.754	0.000	0.000
1.225	2.584	0.734	7.023	1.574	2.426	0.000	0.000
1.337	2.308	0.656	6.273	1.406	2.166	0.000	0.000
1.450	2.085	0.592	5.666	1.270	1.956	0.000	0.000
1.562	1.899	0.540	5.162	1.157	1.783	0.000	0.000
1.674	1.777	0.467	4.749	1.064	1.640	0.029	0.000
1.787	1.672	0.406	4.399	0.985	1.519	0.054	0.000
1.899	1.576	0.357	4.094	0.917	1.414	0.071	0.000
2.012	1.489	0.318	3.827	0.857	1.322	0.082	0.000

Figure 6 AW-101 Dilution @ 40 C

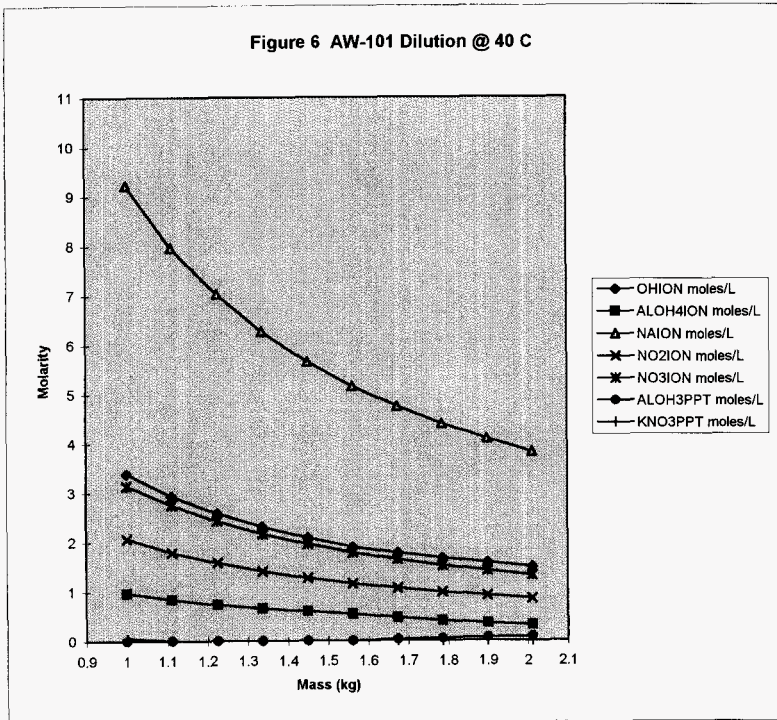
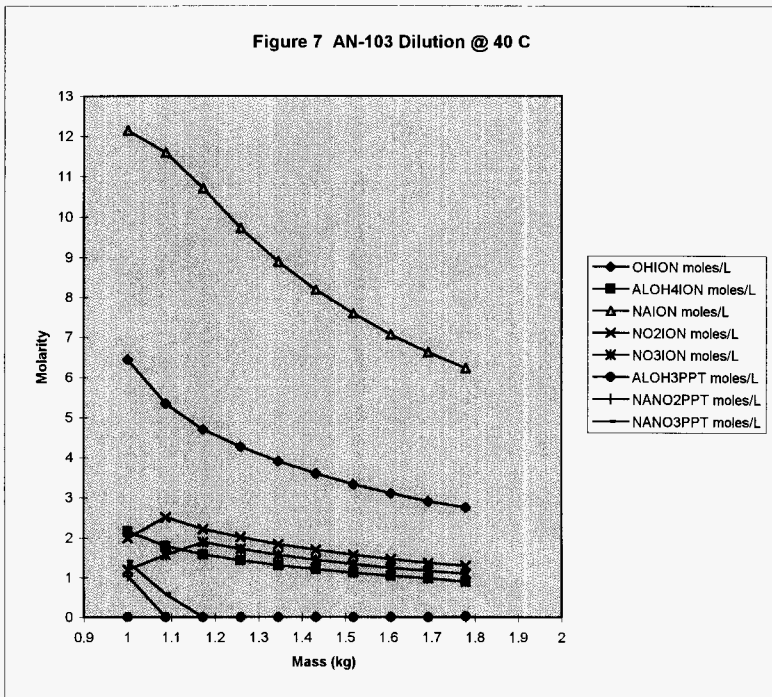


Table 7 AN-103 Dilution @ 40 C

Mass kg	OHION moles/L	ALOH4ION moles/L	NAION moles/L	NO2ION moles/L	NO3ION moles/L	ALOH3PPT moles/L	NANO2PPT moles/L	NANO3PPT moles/L
1.000	6.445	2.162	12.143	1.995	1.201	0.000	1.043	1.405
1.086	5.345	1.793	11.596	2.520	1.570	0.000	0.000	0.587
1.173	4.699	1.576	10.703	2.215	1.890	0.000	0.000	0.000
1.259	4.268	1.432	9.721	2.012	1.714	0.000	0.000	0.000
1.346	3.905	1.310	8.895	1.841	1.567	0.000	0.000	0.000
1.432	3.598	1.207	8.193	1.696	1.443	0.000	0.000	0.000
1.519	3.335	1.119	7.594	1.572	1.337	0.000	0.000	0.000
1.605	3.107	1.042	7.073	1.465	1.245	0.000	0.000	0.000
1.692	2.908	0.975	6.619	1.371	1.165	0.000	0.000	0.000
1.778	2.758	0.896	6.229	1.290	1.096	0.021	0.000	0.000

Figure 7 AN-103 Dilution @ 40 C



2.1.2 Chemistry of Phase 1 Envelope B

Since this supernate is suitable for staging without dilution, it was not modeled. Part of AY-101 is retrieved for Phase 1 P-o-C batches; a third batch is retrieved at the end of the extension.

2.1.3 Chemistry of Phase 1 Envelope C

Reliable speciation data for the organics in Envelope C is not available, so the dilution of Envelope C was not modeled. If the species were known, they would also have to be present in the ESP database. The precipitation phenomenon has been observed in the laboratory with some samples. Further testing is advisable to identify potential problems.

2.2 LOW-ACTIVITY WASTE PRIVATE CONTRACTOR OPERATIONS

Information pertaining to the processes within the Phase 1 private contractor envelope will be available at some future date. The DOE has delegated to private contractors the responsibility for selecting and deploying their own process technology. Consequently, the PPTB does not address private contractor technology specifics, as it would in a more highly developed flowsheet.

The following discussion pertains to the process block diagram depicted Figure 8. Compliance with request for privatization (RFP) requirements has been the primary objective in developing this block diagram and the associated mass balances. The mass balance in Table 8 is for the first batch only, but is typical. A complete set of 24 batch mass balances is provided in Appendix B.

Each process block is geared toward defining "what" the private contractor is required to accomplish rather than "how". Each column of process blocks pertains to an intermediate product, LAW product, or secondary product that the private contractor is returning to the DOE. Some of the streams in Figure 8 are not actual process streams, since this is not a true process flow diagram. These streams are for mass balance purposes only.

While supernate is intended to be a liquid, entrainment of some solids with the LAW is inevitable. The solids come from inadvertent resuspension during retrieval, and possibly from precipitation during dilution. The precipitation phenomenon was discussed previously.

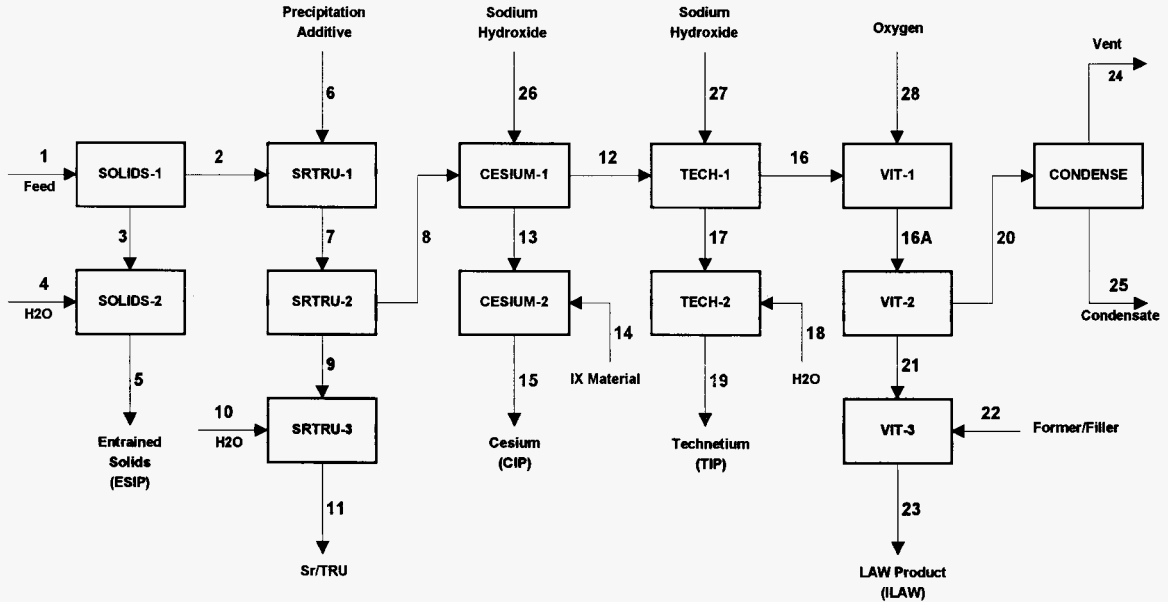
It is incumbent on the operating contractor to ensure that a visible sludge layer of settleable solids occupies no more than 5 vol% of the total transfer, as required by the Request for Proposals (DOE-RL 1996). Non-settling solids (cloudiness) may be present in some transfers nevertheless.

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Since current inventory and DST supernate projections are lacking solids composition information for many DSTs of interest, and since the extent of entrainment is a matter of conjecture, Stream 1 is assigned a "SOLIDS" component equivalent to 1 wt% of the supernate. The solids have an assigned 2.5 spg. There is no direct correlation between wt% solids and vol% settled solids since the latter depends on the extent of thickening. Based on experimentally observed "fluffing", 1 wt% solids should be around 3 vol% settled solids, which is within the RFP requirement of <5 vol% settled solids.

Stream 1 of Figure 8 is the transfer of custody to the private contractor's receiving tank (AP-106 or AP-108). As discussed above, the feed staging plan has identified 24 discrete feed batches for Phase 1 LAW processing, 12 batches for each contractor. The content of the batches (sans the "SOLIDS" component) was previously tabulated in Tables 2a and 2b.

Figure 8 Phase 1 Private Contrator LAW Processing



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Table 8 Mass Balance -- Phase 1 LAW -- Batch PC1/1 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.34E+06	3.33E+06	1.65E+04	4.05E+05	4.22E+05		3.33E+06	3.33E+06		
Density (g/L)	1.44E+03	1.44E+03	1.44E+03	1.00E+03	1.02E+03		1.44E+03	1.44E+03		
Total Mass Flow (kg)	4.82E+06	4.79E+06	2.38E+04	4.05E+05	4.29E+05		4.79E+06	4.79E+06		
RADIONUCLIDES (Ci)										
Cesium	1.03E+06	1.03E+06	5.10E+03		5.10E+03		1.03E+06	1.03E+06		
Strontium	6.62E+03	6.59E+03	3.27E+01		3.27E+01		6.59E+03	6.59E+03		
Technetium	2.71E+02	2.70E+02	1.34E+00		1.34E+00		2.70E+02	2.70E+02		
TRU	2.39E+01	2.38E+01	1.18E-01		1.18E-01		2.38E+01	2.38E+01		
CHEMICALS (kg)										
AGP	8.72E-08	8.69E-08	4.31E-10		4.31E-10		8.68E-08	8.66E-08		
AL(OH) ₃	3.43E+05	3.41E+05	1.69E+03		1.69E+03		3.41E+05	3.41E+05		
AM ₃	8.99E-04	8.94E-04	4.44E-06		4.44E-06		8.94E-04	8.94E-04		
AS ₅	8.40E-03	8.36E-03	4.15E-05		4.15E-05		8.36E-03	8.36E-03		
B ₄ 3	1.52E-01	1.51E-01	7.51E-04		7.51E-04		1.51E-01	1.51E-01		
BA ₂	2.89E-02	2.87E-02	1.43E-04		1.43E-04		2.87E-02	2.87E-02		
BE ₂	1.43E-02	1.44E-02	7.17E-05		7.17E-05		1.44E-02	1.44E-02		
BI ₃	2.61E-06	2.60E-06	1.29E-08		1.29E-08		2.60E-06	2.60E-06		
C-14	1.06E-05	1.06E-05	5.25E-08		5.25E-08		1.06E-05	1.06E-05		
CA ₂	7.30E-01	7.27E-01	3.61E-03		3.61E-03		7.27E-01	7.27E-01		
CD ₂	1.39E-01	1.39E-01	6.87E-04		6.87E-04		1.39E-01	1.39E-01		
CL	1.81E+04	1.81E+04	8.96E+01		8.96E+01		1.81E+04	1.81E+04		
CL ₂										
CO ₂										
CO ₃ -2	4.83E+04	4.81E+04	2.39E+02		2.39E+02		4.81E+04	4.81E+04		
CR(OH) ₃	3.27E+03	3.25E+03	1.61E+01		1.61E+01		3.25E+03	3.25E+03		
CS ₄	1.19E+01	1.19E+01	5.89E-02		5.89E-02		1.19E+01	1.19E+01		
CU ₂	1.74E-07	1.73E-07	8.58E-10		8.58E-10		1.73E-07	1.73E-07		
F ₂	7.58E+02	7.54E+02	3.74E+00		3.74E+00		7.54E+02	7.54E+02		
FE ₃	2.31E+01	2.30E+01	1.14E-01		1.14E-01		2.30E+01	2.30E+01		
HEO	3.00E+06	2.98E+06	1.48E+04	4.05E+05	4.20E+05		2.98E+06	2.98E+06		
K ₂	1.27E+04	1.26E+04	6.27E+01		6.27E+01		1.26E+04	1.26E+04		
Mg ₂	8.44E-01	8.40E-01	4.17E-03		4.17E-03		8.40E-01	8.40E-01		
MN ₄	4.49E-01	4.47E-01	2.22E-03		2.22E-03		4.47E-01	4.47E-01		
MO ₆	3.72E-01	3.71E-01	1.84E-03		1.84E-03		3.71E-01	3.71E-01		
NA ₄	5.79E+05	5.76E+05	2.86E+03		2.86E+03		5.76E+05	5.76E+05		
NI ₃	2.52E+00	2.51E+00	1.25E-02		1.25E-02		2.51E+00	2.51E+00		
NO ₂										
NO ₃	2.51E+05	2.49E+05	1.24E+03		1.24E+03		2.49E+05	2.49E+05		
NO ₃ -3	4.08E+05	4.06E+05	2.01E+03		2.01E+03		4.06E+05	4.06E+05		
NP ₄	2.17E-04	2.16E-04	1.07E-06		1.07E-06		2.16E-04	2.16E-04		
O ₂										
OH	1.29E+05	1.28E+05	6.36E+02		6.36E+02		1.28E+05	1.28E+05		
PB ₄	3.12E-01	3.10E-01	1.54E-03		1.54E-03		3.10E-01	3.10E-01		
PO ₄ -3	5.21E+03	5.18E+03	2.57E+01		2.57E+01		5.18E+03	5.18E+03		
PL ₄	2.87E-01	2.85E-01	1.42E-03		1.42E-03		2.85E-01	2.85E-01		
SE ₆	3.47E-05	3.46E-05	1.72E-07		1.72E-07		3.46E-05	3.46E-05		
SI ₄	1.81E+00	1.81E+00	8.96E-03		8.96E-03		1.81E+00	1.81E+00		
SN ₄	4.35E-06	4.32E-06	2.15E-08		2.15E-08		4.32E-06	4.32E-06		
SO ₄ -2	1.40E+04	1.39E+04	6.91E+01		6.91E+01		1.39E+04	1.39E+04		
SM ₂	4.76E-02	4.74E-02	2.35E-04		2.35E-04		4.74E-02	4.74E-02		
TO ₄	2.63E+01	2.61E+01	1.30E-01		1.30E-01		2.61E+01	2.61E+01		
TI ₄	8.79E-08	8.69E-08	4.31E-10		4.31E-10		8.69E-08	8.69E-08		
TOC	8.44E+03	8.40E+03	4.17E+01		4.17E+01		8.40E+03	8.40E+03		
UO ₂ -2	1.12E+00	1.11E+00	5.51E-03		5.51E-03		1.11E+00	1.11E+00		
ZN ₄	4.35E-06	4.32E-06	2.15E-08		2.15E-08		4.32E-06	4.32E-06		

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Table 8 Mass Balance -- Phase 1 LAW -- Batch PC1/1 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.81E+04	4.81E+02	4.76E+04		4.76E+04		4.81E+02	4.81E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
AG00										
AL2O3										
AM2O3										
AS2O3										
B2O3										
BAO										
BE0										
BI2O3										
CAO										
CO										
CR2O3										
CS2O										
CUO										
FE2O3										
FORMER										
HAHAT										
K2O										
MOO										
MNO2										
MNO3										
NA2O										
NI2O3										
NPO2										
P2O3										
PBO2										
PLUO2										
SEO3										
SI02										
SN02										
SU3										
SOLIDS	4.81E+04	4.81E+02	4.76E+04		4.76E+04		4.81E+02	4.81E+02		
SRO										
TC2O7										
TIO2										
UO3										
ZRO2										

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Table 8 Mass Balance -- Phase 1 LAW -- Batch PCI/1 (6 sheets)

STREAM NAME LIQUID COMPONENTS	11	12	13	14	15	16	16A	17	18	19
Volume (L)		3.33E+06	3.03E+03		3.03E+03	3.33E+06	4.80E+06		1.00E-09	1.00E-09
Density (g/L)		1.44E+03	3.33E+03		3.33E+03	1.44E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.79E+06	1.01E+04		1.01E+04	4.79E+06	4.80E+06		1.00E-09	1.00E-09
RADIOISOTOPES (Ci)										
Cesium		4.42E+03	1.02E+06		1.02E+06	4.42E+03				
Strontium		6.59E+03				6.59E+03				
Technetium		2.67E+02	2.71E+00		2.71E+00	2.67E+02				
TRU		2.38E+01				2.38E+01				
CHEMICALS (kg)										
Ag+		8.69E-08				8.69E-08				
AL(OH) ₄ ⁻		3.41E+05				3.41E+05				
AsH ₃		8.94E-04				8.94E-04				
AsH ₅		8.36E-03				8.36E-03				
BH ₃		1.51E-01				1.51E-01				
BAH ₂		2.87E-02				2.87E-02				
BEH ₂		1.44E-02				1.44E-02				
BiH ₃		2.60E-06				2.60E-06				
C-14		1.06E-05				1.06E-05				
CaH ₂		7.27E-01				7.27E-01				
CD ₂		1.39E-01				1.39E-01				
Cl ₂		1.81E+04				1.81E+04				
Cl ₂							1.81E+04			
CO ₂							6.60E+04			
CO ₃ ⁻²		4.81E+04				4.81E+04				
CR(OH) ₄ ⁻		3.25E+03				3.25E+03				
CSH ⁺		5.10E-02	1.18E+01		1.18E+01	5.10E-02				
CUH ₂		1.73E-07				1.73E-07				
F ⁻		7.54E+02				7.54E+02				
F ₂							7.54E+02			
FEH ₃		2.30E+01				2.30E+01				
H ₂ O		2.98E+06				2.98E+06	3.18E+06		1.00E-09	1.00E-09
K ⁺		1.26E+04				1.26E+04				
MgH ₂		8.40E-01				8.40E-01				
MNH ₄		4.47E-01				4.47E-01				
NDH ₆		3.71E-01				3.71E-01				
Na ⁺		5.76E+03	5.79E+03		5.79E+03	5.76E+03				
NH ₃		2.51E+00				2.51E+00				
NO ₂							5.50E+05			
NO ₂		2.49E+05				2.49E+05				
NO ₃		4.06E+05				4.06E+05				
NP ₄		2.16E-04				2.16E-04				
O ₂							9.85E+05			
OH ⁻		1.29E+05	4.28E+03		4.28E+03	1.29E+05				
OH ⁻		3.10E-01				3.10E-01				
PO ₄ ⁻³		5.18E+03				5.18E+03				
PJH ₄		2.86E-01				2.86E-01				
SEH ₆		3.46E-05				3.46E-05				
SiH ₄		1.81E+00				1.81E+00				
SiH ₄		4.32E-06				4.32E-06				
SO ₄ ⁻²		1.39E+04				1.39E+04				
SRH ₂		4.74E-02				4.74E-02				
TCO ₄		2.59E+01	2.63E-01		2.63E-01	2.59E+01				
TIH ₄		8.69E-08				8.69E-08				
TiC		8.40E+03				8.40E+03				
UO ₂ ⁺²		1.11E+00				1.11E+00				
ZnH ₄		4.32E-06				4.32E-06				

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Table 8 Mass Balance -- Phase 1 LAW -- Batch PCI/1 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.81E+02		5.79E+03	5.79E+03	4.81E+02	9.93E+05			
RADIONUCLIDES (Ci)										
Cesium							4.42E+03			
Strontium							6.59E+03			
Technetium							2.67E+02			
TRU							2.36E+01			
CHEMICALS (kg)										
AC2O							9.33E-08			
AL2O3							1.83E+05			
AM2O3							9.83E-04			
AS2O5							1.28E-02			
B2O3							4.87E-01			
BAO							3.21E-02			
BeO							4.01E-02			
BI2O3							2.90E-06			
CaO							1.02E+00			
CO							1.58E-01			
CR2O3							2.06E+03			
CS2O							5.40E-02			
ClO							2.16E-07			
FE2O3							3.28E+01			
FORMER										
THAMAT				5.79E+03	5.79E+03					
K2O							1.52E+04			
MO							1.39E+00			
MNO2							7.08E-01			
MCO3							5.56E-01			
NA2O							7.77E+05			
NI2O3							3.94E+00			
NP02							2.45E-04			
P2O5							3.87E+03			
PBO2							3.58E-01			
PUO2							3.24E-01			
SE03							5.56E-05			
SI02							3.86E+00			
SN02							5.49E-06			
SO3							1.16E+04			
SOLIDS		4.81E+02				4.81E+02				
SRO							5.58E-02			
TC2O7							2.46E+01			
TI02							1.45E-07			
UC3							1.18E+00			
ZRO2							5.84E-06			

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 TRWS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table 8 Mass Balance -- Phase 1 LAW -- Batch PCI/1 (6 sheets)

STREAM NAME LIQUID COMPONENTS	20	21	22	23	24	25	26	27	28
Volume (L)	4.80E+06				1.62E+06	3.18E+06	3.02E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	4.80E+06				1.62E+06	3.18E+06	1.01E+04	1.00E-09	1.00E+06
RADIOISOTOPES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AG+									
AL(OH) ₄ ⁻									
AM+3									
AS+5									
B+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL									
CL2	1.81E+04				1.81E+04				
CO2	6.60E+04				6.60E+04				
CO3 ⁻²									
CR(OH) ₄ ⁻									
CS+									
CU+2									
F-									
FE	7.54E+02				7.54E+02				
FE+3									
H2O	3.18E+06					3.18E+06			
K+									
MG+2									
MN+4									
MO+6									
NA+									
NI+3									
NO2	5.50E+05				5.50E+05		5.79E+03	5.75E-10	
NO2-									
NO3-									
NP+4									
O2	9.85E+05				9.85E+05		4.28E+03	4.25E-10	1.00E+06
OH-									
PBM+4									
PO4 ⁻³									
PU+4									
SE+6									
SI+4									
SO4 ⁻²									
SO4 ⁻²									
SR+2									
TO2 ⁻									
TI+4									
TiC									
UO2 ⁺²									
ZR+4									

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Table 8 Mass Balance -- Phase 1 LAW -- Batch PC1/1 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		9.92E+05	3.61E+06	4.60E+06					
RADIONUCLIDES (Ci)									
Cesium		4.42E+03		4.42E+03					
Strontium		6.59E+03		6.59E+03					
Technetium		2.67E+02		2.67E+02					
TRU		2.36E+01		2.36E+01					
CHEMICALS (kg)									
AC2O		9.33E-08		9.33E-08					
AL2O3		1.83E+05		1.83E+05					
AM2O3		9.83E-04		9.83E-04					
AS2O3		1.28E-02		1.28E-02					
B2O3		4.87E-01		4.87E-01					
B4O		3.21E-02		3.21E-02					
BE2O		4.01E-02		4.01E-02					
BI2O3		2.90E-06		2.90E-06					
CAO		1.02E+00		1.02E+00					
CO		1.58E-01		1.58E-01					
CR2O3		2.06E+03		2.06E+03					
CS2O		5.40E-02		5.40E-02					
CUO		2.16E-07		2.16E-07					
FE2O3		3.28E+01		3.28E+01					
FORMER TDMAT			3.61E+06	3.61E+06					
K2O		1.52E+04		1.52E+04					
MO		1.39E+00		1.39E+00					
MNO2		7.08E-01		7.08E-01					
MCO3		5.56E-01		5.56E-01					
NA2O		7.77E+05		7.77E+05					
NI2O3		3.54E+00		3.54E+00					
NFO2		2.43E-04		2.43E-04					
P2O5		3.87E+03		3.87E+03					
PBO2		3.58E-01		3.58E-01					
PUO2		3.24E-01		3.24E-01					
SEO3		5.56E-05		5.56E-05					
SI02		3.86E+00		3.86E+00					
SN02		5.49E-06		5.49E-06					
SZ5		1.16E+04		1.16E+04					
SOLIDS		4.81E+02		4.81E+02					
SRO		5.58E-02		5.58E-02					
TC2O7		2.46E+01		2.46E+01					
TIO2		1.45E-07		1.45E-07					
UC3		1.18E+00		1.18E+00					
ZRO2		5.84E-06		5.84E-06					

See other Phase 1 LAW mass balances in Appendix B

2.2.1 Entrained Solids Intermediate Product

Process block SOLIDS-1 thickens entrained solids, distributing 1% of the solids to Stream 2 and 99% to the thickened Stream 3. Stream 3 is allowed to contain <60 g Na per kg of solid, the Specification 10⁶ allowance for sodium in the Entrained Solids Intermediate Product (ESIP). The extent to which liquids (and sodium) can be displaced from a thickened sludge is limited 60 to 70 vol% by the natural void fraction of a porous bed, which is in the range of 30 to 40 vol%. Figure 9 illustrates the residual Na content in a sludge as a function of the displacement fraction (volume fraction of sludge occupied by solid) and the density of the solid. For a sludge containing 7M Na liquid and 2.5 spg solids, the solids must displace at least 50 vol% of a sludge to achieve the desired residual sodium content.⁷

The Stream 3 emerging from process block SOLIDS-1 is much too dense and viscous for pipeline transfer; bulk density of 1.9 kg/L or higher is typical. Process block SOLIDS-2 dilutes the high bulk density sludge with water to yield slurries containing 10 wt% solids, which should be in the range of 20 to 30 settled vol%⁸, and <1.5 spg in accordance with Specification 9. ESIP returning from PC1's twelve batches of supernate will contain 420,000 kgs of solids in 3,700,000 L of liquid. PC2 returns virtually the same amount.

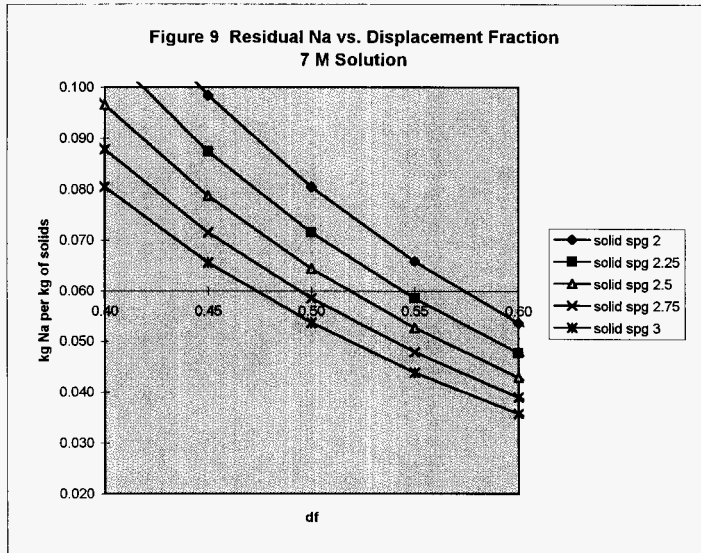
⁶All specifications in the PPTB have reference to Specifications 1 through 10 in the RFP (DOE 1996). Typical washed solids contain more sodium than Specification 10 allows. For the PPTB, Specification 10 was interpreted to apply to the interstitial liquor only.

⁷Obviously, sludge thickening by itself cannot displace enough sodium to satisfy the requirement if the interstitial liquid is highly concentrated. Additional measures such as washing would be required.

⁸There is a correlation between wt% solids and vol% displaced by solids, but there is no correlation with vol% settled solids. Therefore, given a wt% solids, one can only estimate the vol% settled solids.

Table 9 Displacement of 7M Na Interstitial Liquid by Solids

df	solid spg 2	solid spg 2.25	solid spg 2.5	solid spg 2.75	solid spg 3
Kgs Residual Sodium per Kg of solid					
0.01	7.970	7.084	6.376	5.796	5.313
0.03	2.603	2.314	2.082	1.893	1.735
0.05	1.530	1.360	1.224	1.112	1.020
0.10	0.725	0.644	0.580	0.527	0.483
0.15	0.456	0.405	0.365	0.332	0.304
0.20	0.322	0.286	0.258	0.234	0.215
0.25	0.242	0.215	0.193	0.176	0.161
0.30	0.188	0.167	0.150	0.137	0.125
0.35	0.150	0.133	0.120	0.109	0.100
0.40	0.121	0.107	0.097	0.088	0.081
0.45	0.098	0.087	0.079	0.072	0.066
0.50	0.081	0.072	0.064	0.058	0.053
0.55	0.066	0.058	0.051	0.048	0.044
0.60	0.053	0.048	0.043	0.039	0.036
0.65	0.043	0.039	0.035	0.032	0.029
0.70	0.035	0.031	0.028	0.025	0.023
0.75	0.027	0.024	0.021	0.020	0.018



Na content of <0.06kgs Na/kgs solids required by Entrained Solids specification

2.2.2 Strontium/TRU Intermediate Product

Supernate that would cause either ^{90}Sr or TRU to exceed ILAW concentration limits (20 Ci/m³ or 100 nCi/g, respectively) invokes process blocks SRTRU-1 through -3. SRTRU-1 is a coprecipitation operation. Process blocks SRTRU-2 and SRTRU-3 are analogous to SOLIDS-1 and SOLIDS-2, i.e., a thickening step to displace sodium from the precipitate, and a dilution step to prepare slurry for return to the operating contractor. Process block SRTRU-2 distributes 1% of the Strontium/TRU solids to Stream 8 and 99% to Stream 9. The interstitial liquid in Stream 9 contains <60 g Na per kg of solid, the Specification 10 allowance for sodium in Strontium/TRU Intermediate Product. Process block SRTRU-3 dilutes the Strontium/TRU high density sludge with water to yield slurries containing 10 wt% solids, which will be in the range of 20 to 30 settled vol%, and <1.5 spg in accordance with Specification 9. PC2 returns 12,000 L Sr/TRU intermediate product. More than likely it would be combined with the ESIP.

2.2.3 Cesium Intermediate Product

Supernate that would cause the ILAW concentration of ^{137}Cs to exceed 3 Ci/m³ invokes process blocks CESIUM-1 and -2. Process block CESIUM-1 removes the requisite amount of radiocesium. Process block CESIUM-2 produces the dry, free-flowing cesium product (Stream 15). Specification 10 allows for a total of 10 kg of miscellaneous oxides (excluding sodium and silicon) to be added to the intermediate product streams, per metric ton of Na in the feed. The entire allowance of miscellaneous oxides (Stream 14) is added through process block CESIUM-2 to become part of the CIP. Process block CESIUM-1 also distributes 1% of the technetium and 10 kg Na per metric ton of feed sodium to Stream 13, the maximum allowance in Specification 4 and Specification 10, respectively. PC2 will return 31 standard Cs packages, based on the maximum heat load of 1,500 watts per package.

2.2.4 Technetium Intermediate Product (TIP)

Supernate that would cause the ILAW concentration of ^{99}Tc to exceed 0.3 Ci/m³ invokes process block TECH-1, which removes the requisite amount of radiotechnetium. Process block TECH-1 distributes 10 kg Na per metric ton of feed sodium to Stream 17, the maximum allowance in Specification 10. Process block TECH-1 also distributes all of the remaining ^{137}Cs to Stream 16 so that Stream 19 will contain less than 0.0015 Ci/L of gamma emitters, as required per Specification 5. Only four of PC2's twelve batches require Tc treatment; 15,000 L of Tc concentrate are returned.

2.2.5 Immobilized Low Activity Waste

After the removal of entrained solids, strontium/TRU, cesium, and technetium as needed, the pretreated LAW (Stream 16) is suitable for immobilization. Process block VIT-1 volatilizes water, fluoride, iodide, chloride, carbonate, nitrite and nitrate to their gaseous equivalent, and converts non-volatile constituents to their oxide equivalent. Process block VIT-2 is a gas/solid separation that routes the volatile species to condensation and the oxide equivalents to immobilization. The final packaged volume is dictated by the amount of sodium in the feed stream (3.18 m³/1,000 kg sodium for Envelopes A and C, and 7.95 m³/1,000 kg sodium for Envelope B). The final packaged volume is filled to 80 vol% with ILAW and 20 vol% with filler. To finish the immobilization, process block VIT-3 adds a sufficient mass of former/filler material to produce a final bulk density of 2.5 kg/L within the waste package. The addition of former/filler material is obviously sensitive to the value assumed for the bulk density.

The final packaged volume divided by the standard package volume (2.59 m³) yields the ILAW standard package count. PC1 produces 6745 packages; PC2 produces 6412 packages. The difference is primarily due to the larger volume of Envelope B processed by PC1.

2.2.6 Condensation

The volatile species directed to Stream 20 by process block VIT-2 are separated into the non-condensables (Stream 24) and the condensables (Stream 25) by process block CONDENSE.

2.3 HIGH-LEVEL WASTE PRETREATMENT AND STAGING

The operating contractor pretreats and stages Envelope D HLW sludge to one private contractor. The pretreatment process entails separating water soluble components from sludges by washing, settling, and decanting. The HLW feed staging plan (Manuel 1996) identifies three tanks for staging (AZ-101, AZ-102, AY-102). These tanks are involved in a near-term in-tank retrieval test (Project W-151), a retrieval demonstration (Project W-320), and waste consolidation activities (Bacon 1996) that have been integrated with the process flow diagram and mass balance. Pretreatment and staging activities for each tank are described below. Unlike LAW, pretreated HLW is pumped directly from the source tanks to the private contractor's facility.

Appendix D tabulates the inventory of AZ-101, AZ-102, and AY-102, as well as C-106 (which is retrieved into AY-102). Appendix D also shows how the inventory distributes between liquid and solid. Due to physical characteristics, the susceptibility of these solids to retrieval by mixer-pump technology differs from tank to tank. Retrieval efficiencies with two 300 hp pumps have been estimated for each of the Envelope D source tanks, as noted below. The retrievable fraction is 95% of the liquids, plus one of the following for solids: 90% of AZ-101, 60% of AZ-102, 36% of AY-102, and 99% of C-106. The retrievable fraction comprises Stream 1 on the following sludge washing flowsheets.

To be conservative, all of the solids in a tank were assumed to occupy a 20 wt% settled solids layer, and the best combinations of wash repetitions and wash ratio were determined to optimize schedule and wash volume (Washenfelder 1996). The wash volume in the following flowsheets is sized for complete mobilization, even though the feed stream itself is based on a fractional retrieval efficiency. Consequently, the wash volume depicted in these flowsheets is adequate even if actual solid retrieval efficiency is better than expected.

The residual waste in these tanks is composited with the Phase 2 pretreatment feed stream.

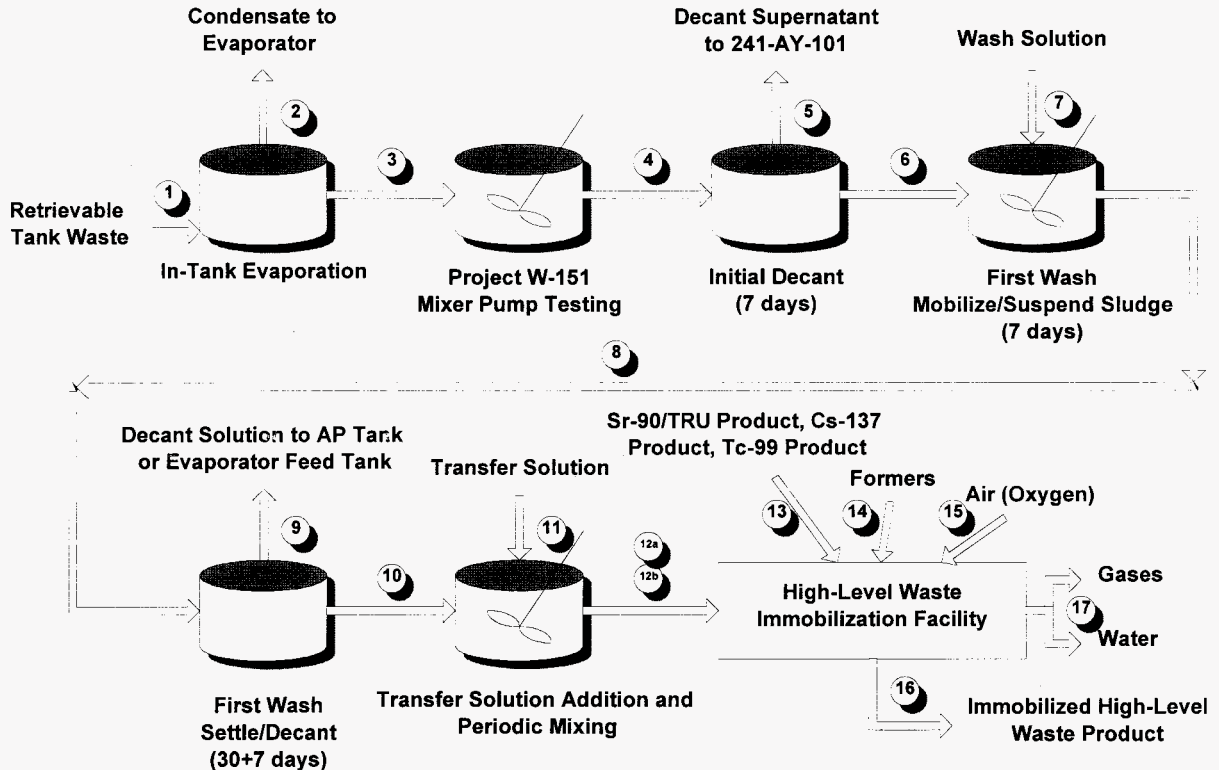
2.3.1 AZ-101

Figure 10 is the process flow diagram⁹ for AZ-101 waste and Table 10 shows the associated mass balance for the retrievable portion of the waste. Stream 1 consists of 95% of the liquids and 90% of the solids in AZ-101. Stream 1 supernates concentrate to 5M Na (Stream 3) by in-tank evaporation prior to an in-tank mixer pump test. The mobilized slurry settles and a 20 wt% solids layer (plus 1 ft of supernate liquid) remains (Stream 6), after the balance of the supernate is decanted to AY-101 (Stream 5). The decanted supernate is suitable for Envelope B feed.

A single wash with three volumes of dilute caustic per volume of settled solids, followed by settling and decanting, yields a sludge with sufficiently dilute interstitial liquid (Stream 10). With transfer solution added back to satisfy Specification 8 (HLW feed slurry parameters), AZ-101 produces two 540,000 L (143,000 gal) batches of HLW feed (Stream 12).

⁹Note that this diagram depicts a series of operations in the same tank. Each effluent stream represents the contents of the tank after each operation is completed. The waste does not actually flow from tank to tank.

Figure 10. In-Tank Sludge Washing of Double-Shell Tank 241-AZ-101



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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Total Mass Flow (kg)	4.09E+06	4.02E+05	3.68E+06	3.68E+06	3.05E+06	6.33E+05	1.52E+06	2.15E+06	1.55E+06	6.06E+05
Volume (L)	3.23E+06	4.02E+05	2.88E+06	2.88E+06	2.30E+06	4.79E+05	1.51E+06	2.01E+06	1.44E+06	5.69E+05
Specific Gravity	1.25E+00	1.00E+00	1.28E+00	1.28E+00	1.29E+00	1.28E+00	1.00E+00	1.07E+00	1.07E+00	1.07E+00

Radionuclides (Ci)										
Atr-241	8.21E+02		8.21E+02	8.21E+02	6.80E+02	1.41E+02		1.41E+02	1.01E+02	3.97E+01
C-14	1.79E+02		1.79E+02	1.79E+02	1.48E+02	3.08E+01		3.08E+01	2.21E+01	8.67E+00
Qtr-244	1.82E+01		1.82E+01	1.82E+01	1.51E+01	3.13E+00		3.13E+00	2.25E+00	8.80E-01
Cs-137	5.78E+06		5.78E+06	5.78E+06	4.75E+06	9.94E+05		9.94E+05	7.15E+05	2.80E+05
Ba-137	5.50E+06		5.50E+06	5.50E+06	4.55E+06	9.43E+05		9.43E+05	6.79E+05	2.66E+05
Eu-154										
Np-237										
Plu-239	1.03E+00		1.03E+00	1.03E+00	8.52E-01	1.77E-01		1.77E-01	1.27E-01	4.98E-02
Plu-240										
Plu-241										
Sr-90	2.70E+05		2.70E+05	2.70E+05	2.24E+05	4.65E+04		4.65E+04	3.34E+04	1.31E+04
Y-90	2.70E+05		2.70E+05	2.70E+05	2.24E+05	4.65E+04		4.65E+04	3.34E+04	1.31E+04
Tc-99	6.41E+02		6.41E+02	6.41E+02	5.31E+02	1.10E+02		1.10E+02	7.92E+01	3.10E+01
Total Curies	1.18E+07		1.18E+07	1.18E+07	9.79E+06	2.03E+06		2.03E+06	1.46E+06	5.72E+05

Chemicals (kg)										
Ag+										
Am+3	2.39E-01		2.39E-01	2.39E-01	1.98E-01	4.11E-02		4.11E-02	2.96E-02	1.16E-02
As+5	2.51E+00		2.51E+00	2.51E+00	2.08E+00	4.32E-01		4.32E-01	3.11E+01	1.22E-01
B+3	8.53E-01		8.53E-01	8.53E-01	7.06E-01	1.47E-01		1.47E-01	1.05E-01	4.13E-02
Be+2	9.07E-02		9.07E-02	9.07E-02	7.51E-02	1.56E-02		1.56E-02	1.12E-02	4.39E-03
Be+2	1.03E-03		1.03E-03	1.03E-03	8.51E-04	1.77E-04		1.77E-04	1.27E-04	4.97E-05
Bi+3										
Ca+2	1.52E+00		1.52E+00	1.52E+00	1.26E+00	2.61E-01		2.61E-01	1.88E-01	7.36E-02
Ca+2	5.59E-02		5.59E-02	5.59E-02	4.63E-02	9.61E-03		9.61E-03	6.91E-03	2.70E-03
Ce+3	2.30E+00		2.30E+00	2.30E+00	1.90E+00	3.95E-01		3.95E-01	2.84E-01	1.11E-01
Cr+3	2.25E-04		2.25E-04	2.25E-04	1.86E-04	3.86E-05		3.86E-05	2.78E-05	1.09E-05
Co+3	7.12E-04		7.12E-04	7.12E-04	5.90E-04	1.22E-04		1.22E-04	8.80E-05	3.44E-05
Co+	2.60E+02		2.60E+02	2.60E+02	2.15E+02	4.46E+01		4.46E+01	3.21E+01	1.25E+01
Cr+2	1.98E-01		1.98E-01	1.98E-01	1.64E-01	3.40E-02		3.40E-02	2.44E-02	9.57E-03
Eu+3	4.60E-01		4.60E-01	4.60E-01	3.81E-01	7.90E-02		7.90E-02	5.69E-02	2.22E-02
Hg+2										
K+	6.48E+02		6.48E+02	6.48E+02	5.37E+02	1.11E+02		1.11E+02	8.01E+01	3.13E+01
La+3	1.73E-01		1.73E-01	1.73E-01	1.43E-01	2.97E-02		2.97E-02	2.14E-02	8.34E-03
Li+	4.28E-01		4.28E-01	4.28E-01	3.54E-01	7.35E-02		7.35E-02	5.28E-02	2.07E-02
Mg+2	8.24E-02		8.24E-02	8.24E-02	6.83E-02	1.42E-02		1.42E-02	1.02E-02	3.99E-03
Mn+4	4.21E-02		4.21E-02	4.21E-02	3.48E-02	7.23E-03		7.23E-03	5.20E-03	2.04E-03
Mo+6	1.31E+01		1.31E+01	1.31E+01	1.08E+01	2.24E+00		2.24E+00	1.61E+00	6.31E-01
Na+	3.31E+05		3.31E+05	3.31E+05	2.74E+05	5.69E+04	3.83E+03	6.07E+04	4.36E+04	1.71E+04
Ni+3	1.21E-01		1.21E-01	1.21E-01	1.00E-01	2.08E-02		2.08E-02	1.49E-02	5.85E-03
Np+4										
Pb+4	9.07E-01		9.07E-01	9.07E-01	7.51E-01	1.56E-01		1.56E-01	1.12E-01	4.39E-02
Plu+4	1.66E-02		1.66E-02	1.66E-02	1.37E-02	2.85E-03		2.85E-03	8.02E-03	3.02E-03
Re+7	2.13E-01		2.13E-01	2.13E-01	1.77E-01	3.67E-02		3.67E-02	2.64E-02	1.03E-02
Rh+3	1.53E+00		1.53E+00	1.53E+00	1.27E+00	2.63E-01		2.63E-01	1.89E-01	7.40E-02
Ru+3	7.25E-01		7.25E-01	7.25E-01	6.04E-01	1.25E-01		1.25E-01	9.01E-02	3.53E-02
Sb+5	1.98E+00		1.98E+00	1.98E+00	1.64E+00	3.40E-01		3.40E-01	2.44E-01	9.57E-02
Se+6	3.71E+00		3.71E+00	3.71E+00	3.07E+00	6.37E-01		6.37E-01	4.59E-01	1.79E-01
Si+4	5.37E+01		5.37E+01	5.37E+01	4.45E+01	9.24E+00		9.24E+00	6.64E+00	2.60E+00

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Chemicals (kg) (cont.)										
SiH4			9.36E+00	9.36E+00	7.75E+00	1.61E+00		1.61E+00	1.16E+00	4.53E-01
Si+2	9.36E+00		3.97E+00	3.97E+00	3.28E+00	6.82E-01		6.82E-01	4.90E-01	1.92E-01
Tet+6	3.21E+00		3.21E+00	3.21E+00	2.65E+00	5.51E-01		5.51E-01	3.96E-01	1.59E-01
Ti+4	1.14E+00		1.14E+00	1.14E+00	9.44E-01	1.96E-01		1.96E-01	1.41E-01	5.52E-02
Ti+3	3.97E+01		3.97E+01	3.97E+01	3.28E+01	6.82E+00		6.82E+00	4.90E+00	1.92E+00
UO2+2	8.81E+00		8.81E+00	8.81E+00	7.30E+00	1.52E+00		1.52E+00	1.09E+00	4.26E-01
V+5	1.37E-01		1.37E-01	1.37E-01	1.13E-01	2.35E-02		2.35E-02	1.69E-02	6.60E-03
W+6										
Zn+2	2.03E-01		2.03E-01	2.03E-01	1.68E-01	3.49E-02		3.49E-02	2.51E-02	9.82E-03
Zn+4										
Al(OH)4-	1.15E+05		1.15E+05	1.15E+05	9.52E+04	1.98E+04		1.98E+04	1.42E+04	5.56E+03
Cl-	5.79E+02		5.79E+02	5.79E+02	4.79E+02	9.95E+01		9.95E+01	7.15E+01	2.80E+01
CO3-2	9.68E+04		9.68E+04	9.68E+04	8.01E+04	1.66E+04		1.66E+04	1.20E+04	4.68E+03
Cr(OH)4-	4.56E+02		4.56E+02	4.56E+02	3.78E+02	7.84E+01		7.84E+01	5.64E+01	2.21E+01
F-	5.63E+03		5.63E+03	5.63E+03	4.67E+03	9.68E+02		9.68E+02	6.98E+02	2.73E+02
I-	3.25E-01		3.25E-01	3.25E-01	2.69E-01	5.59E-02		5.59E-02	4.01E-02	1.57E-02
NO2-	1.92E+05		1.92E+05	1.92E+05	1.60E+05	3.31E+04	6.97E+02	3.38E+04	2.43E+04	9.52E+03
NO3-	2.24E+05		2.24E+05	2.24E+05	1.85E+05	3.85E+04		3.85E+04	2.76E+04	1.08E+04
OH-	3.15E+04		3.15E+04	3.15E+04	2.60E+04	5.41E+03	2.58E+03	7.92E+03	5.79E+03	2.25E+03
PO4-3	3.72E+01		3.72E+01	3.72E+01	3.09E+01	6.39E+00		6.39E+00	4.59E+00	1.80E+00
SO4-2	2.09E+01		2.09E+01	2.09E+01	1.73E+01	3.59E+00		3.59E+00	2.58E+00	1.01E+00
TcO4-	6.24E+01		6.24E+01	6.24E+01	5.17E+01	1.07E+01		1.07E+01	7.71E+00	3.02E+00
H2O	3.08E+06	4.02E+05	2.68E+06	2.68E+06	2.22E+06	4.61E+05	1.51E+06	1.97E+06	1.42E+06	5.59E+05
Organic Carbon	3.42E+03		3.42E+03	3.42E+03	2.83E+03	5.88E+02		5.88E+02	4.23E+02	1.66E+02
ZrO2·2H2O	1.23E-01		1.23E-01	1.23E-01	1.02E-01	2.11E-02		2.11E-02	1.52E-02	5.93E-03
Hg										
Cl2										
CO2										
F2										
I2										
N2										
NO										
NH3										

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	1.19E+05		1.19E+05	1.19E+05	3.92E+02	1.18E+05		1.18E+05	3.91E+02	1.18E+05
Radionuclides (Ci)										
Am-241	2.51E+04		2.51E+04	2.51E+04	8.29E+01	2.51E+04		2.51E+04	8.27E+01	2.50E+04
C-14	1.40E+01		1.40E+01	1.40E+01	4.60E-02	1.39E+01		1.39E+01	4.59E-02	1.39E+01
Om-244	6.45E+02		6.45E+02	6.45E+02	2.13E+00	6.43E+02		6.43E+02	2.12E+00	6.41E+02
Cs-137	2.16E+05		2.16E+05	2.16E+05	7.14E+02	2.16E+05		2.16E+05	7.11E+02	2.15E+05
Ba-137	2.05E+05		2.05E+05	2.05E+05	6.78E+02	2.05E+05		2.05E+05	6.76E+02	2.04E+05
Eu-154										
Np-237										
Pu-239	4.87E+02		4.87E+02	4.87E+02	1.61E+00	4.85E+02		4.85E+02	1.60E+00	4.84E+02
Pu-240										
Pu-241										
Sm-90	4.67E+06		4.67E+06	4.67E+06	1.54E+04	4.65E+06		4.65E+06	1.54E+04	4.64E+06
Y-90	4.67E+06		4.67E+06	4.67E+06	1.54E+04	4.65E+06		4.65E+06	1.54E+04	4.64E+06
Tc-99	1.32E+02		1.32E+02	1.32E+02	4.36E-01	1.32E+02		1.32E+02	4.35E-01	1.31E+02
Total Curies	9.78E+06		9.78E+06	9.78E+06	3.23E+04	9.75E+06		9.75E+06	3.22E+04	9.72E+06
Chemicals (kg)										
Al+3	1.05E+04	1.05E+04	1.05E+04	3.45E+01	1.04E+04		1.04E+04	3.44E+01	1.04E+04	
Am+3	7.33E+00	7.33E+00	7.33E+00	2.42E-02	7.30E+00		7.30E+00	2.41E-02	7.28E+00	
As+5	1.21E+02	1.21E+02	1.21E+02	3.99E-01	1.21E+02		1.21E+02	3.98E-01	1.20E+02	
B+3	6.39E+01	6.39E+01	6.39E+01	2.11E-01	6.36E+01		6.36E+01	2.10E-01	6.34E+01	
Ba+2	1.57E+02	1.57E+02	1.57E+02	5.19E-01	1.57E+02		1.57E+02	5.17E-01	1.56E+02	
Be+2	3.79E+00	3.79E+00	3.79E+00	1.25E-02	3.78E+00		3.78E+00	1.25E-02	3.77E+00	
Ca+2	5.26E+02	5.26E+02	5.26E+02	1.74E+00	5.24E+02		5.24E+02	1.73E+00	5.22E+02	
Cd+2	1.23E+03	1.23E+03	1.23E+03	4.05E+00	1.22E+03		1.22E+03	4.04E+00	1.22E+03	
Ce+3	2.62E+02	2.62E+02	2.62E+02	8.64E-01	2.61E+02		2.61E+02	8.61E-01	2.60E+02	
Om+3	7.97E-03	7.97E-03	7.97E-03	2.63E-05	7.94E-03		7.94E-03	2.62E-05	7.91E-03	
Co+3	7.52E-04	7.52E-04	7.52E-04	2.48E-06	7.49E-04		7.49E-04	2.47E-06	7.47E-04	
Cr+3	1.71E+02	1.71E+02	1.71E+02	5.65E-01	1.71E+02		1.71E+02	5.63E-01	1.70E+02	
Cs+	9.70E+00	9.70E+00	9.70E+00	3.20E-02	9.67E+00		9.67E+00	3.19E-02	9.64E+00	
Cl+2	9.33E+01	9.33E+01	9.33E+01	3.08E-01	9.30E+01		9.30E+01	3.07E-01	9.27E+01	
Fe+3	2.17E+04	2.17E+04	2.17E+04	7.16E+01	2.16E+04		2.16E+04	7.13E+01	2.15E+04	
K+	6.64E+02	6.64E+02	6.64E+02	2.19E+00	6.62E+02		6.62E+02	2.19E+00	6.60E+02	
La+3	8.20E+02	8.20E+02	8.20E+02	2.71E+00	8.17E+02		8.17E+02	2.70E+00	8.15E+02	
Li+	1.54E+01	1.54E+01	1.54E+01	5.08E-02	1.53E+01		1.53E+01	5.06E-02	1.53E+01	
Mg+2	1.32E+02	1.32E+02	1.32E+02	4.34E-01	1.32E+02		1.32E+02	4.33E-01	1.31E+02	
Mn+4	6.55E+02	6.55E+02	6.55E+02	2.16E+00	6.53E+02		6.53E+02	2.15E+00	6.51E+02	
Mo+6	1.18E+01	1.18E+01	1.18E+01	3.88E-02	1.17E+01		1.17E+01	3.87E-02	1.17E+01	
Na+	3.51E+03	3.51E+03	3.51E+03	1.16E+01	3.50E+03		3.50E+03	1.15E+01	3.49E+03	
Ni+3	9.59E+02	9.59E+02	9.59E+02	3.17E+00	9.56E+02		9.56E+02	3.15E+00	9.53E+02	
Pb+4	1.14E+02	1.14E+02	1.14E+02	3.76E-01	1.14E+02		1.14E+02	3.75E-01	1.13E+02	
Pu+4	7.85E+00	7.85E+00	7.85E+00	2.59E-02	7.83E+00		7.83E+00	2.58E-02	7.80E+00	
Re+7	1.23E+01	1.23E+01	1.23E+01	4.05E-02	1.22E+01		1.22E+01	4.04E-02	1.22E+01	
Rh+3	9.33E+01	9.33E+01	9.33E+01	3.08E-01	9.30E+01		9.30E+01	3.07E-01	9.27E+01	
Ru+3	1.92E+02	1.92E+02	1.92E+02	6.33E-01	1.91E+02		1.91E+02	6.31E-01	1.91E+02	
Sb+5	5.88E+02	5.88E+02	5.88E+02	1.94E+00	5.86E+02		5.86E+02	1.94E+00	5.85E+02	
Se+6	3.86E+02	3.86E+02	3.86E+02	1.27E+00	3.85E+02		3.85E+02	1.27E+00	3.84E+02	
Si+4	1.22E+03	1.22E+03	1.22E+03	4.02E+00	1.21E+03		1.21E+03	4.01E+00	1.21E+03	
Sn+2	1.62E+02	1.62E+02	1.62E+02	5.34E-01	1.61E+02		1.61E+02	5.32E-01	1.61E+02	
Te+6	4.15E+02	4.15E+02	4.15E+02	1.37E+00	4.13E+02		4.13E+02	1.36E+00	4.12E+02	
Th+4	2.66E+02	2.66E+02	2.66E+02	8.78E-01	2.65E+02		2.65E+02	8.75E-01	2.64E+02	
Ti+4	1.43E+02	1.43E+02	1.43E+02	4.70E-01	1.42E+02		1.42E+02	4.69E-01	1.42E+02	
Tl+3	1.43E+03	1.43E+03	1.43E+03	4.70E+00	1.42E+03		1.42E+03	4.69E+00	1.42E+03	

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Chemicals (kg) (cont.)										
UD2+2	1.34E+03		1.34E+03	1.34E+03	4.42E+00	1.34E+03		1.34E+03	4.41E+00	1.33E+03
V+5	5.44E+00		5.44E+00	5.44E+00	1.80E-02	5.43E+00		5.43E+00	1.79E-02	5.41E+00
Zn+2	8.73E+01		8.73E+01	8.73E+01	2.88E-01	8.70E+01		8.70E+01	2.87E-01	8.67E+01
Cl-	2.41E+01		2.41E+01	2.41E+01	7.96E-02	2.40E+01		2.40E+01	7.93E-02	2.40E+01
OD3-2	3.30E+03		3.30E+03	3.30E+03	1.09E+01	3.29E+03		3.29E+03	1.09E+01	3.28E+03
F-	1.33E+02		1.33E+02	1.33E+02	4.39E-01	1.33E+02		1.33E+02	4.38E-01	1.32E+02
I-	2.25E-01		2.25E-01	2.25E-01	7.41E-04	2.24E-01		2.24E-01	7.39E-04	2.23E-01
NO2-	1.52E+03		1.52E+03	1.52E+03	5.02E+00	1.52E+03		1.52E+03	5.00E+00	1.51E+03
NO3-	1.24E+03		1.24E+03	1.24E+03	4.11E+00	1.24E+03		1.24E+03	4.09E+00	1.24E+03
OH-	4.93E+04		4.93E+04	4.93E+04	1.63E+02	4.92E+04		4.92E+04	1.62E+02	4.90E+04
PO4-3	5.02E+01		5.02E+01	5.02E+01	1.66E-01	5.00E+01		5.00E+01	1.65E-01	4.99E+01
SO4-2	5.56E+00		5.56E+00	5.56E+00	1.84E-02	5.55E+00		5.55E+00	1.83E-02	5.53E+00
TcO4-	1.29E+01		1.29E+01	1.29E+01	4.25E-02	1.28E+01		1.28E+01	4.23E-02	1.28E+01
MnO2										
Organic Carbon	1.81E+03		1.81E+03	1.81E+03	5.99E+00	1.81E+03		1.81E+03	5.97E+00	1.80E+03
ZrO2.2H2O	1.33E+04		1.33E+04	1.33E+04	4.39E+01	1.33E+04		1.33E+04	4.38E+01	1.32E+04
Ag2O										
Al2O3										
Am2O3										
As2O3										
B2O3										
BaO										
BeO										
Bi2O3										
CaO										
CdO										
Ce2O3										
On2O3										
Co2O3										
Cr2O3										
Cs2O										
ClO										
Eu2O3										
Fe2O3										
K2O										
La2O3										
Li2O										
MgO										
MnO3										
N2O3										
Ni2O3										
NfO2										
P2O5										
PfO2										
PuO2										
Re2O7										
Rh2O3										
Ru2O3										
Sb2O3										
SeO3										
SiO2										
SO3										
SrO										
Tc2O7										
TcO3										
ThO2										
TiO2										
Tl2O3										

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Chemicals (kg) (cont.)										
UO ₂										
U ₂ O ₅										
WO ₃										
ZrO										
ZrO ₂										

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	11	12	13	14	15	16	17
LIQUID COMPONENTS							
Total Mass Flow (kg)	5.14E+05	1.12E+06	3.40E+04				1.14E+06
Volume (L)	5.16E+05	1.08E+06	1.41E+04				1.14E+06
Specific Gravity	1.00E+00	1.04E+00	2.41E+00				1.00E+00
Radionuclides (Ci)							
Am-241		3.97E+01	7.05E-03				
C-14		8.67E+00	4.09E-04				
Om-244		8.80E-01					
Cs-137		2.80E+05	2.79E+06				
Ba-137		2.66E+05	2.65E+06				
Eu-154			2.42E-02				
Np-237			1.80E-07				
Pu-239	4.98E-02		1.58E-03				
Pu-240			3.94E-04				
Pu-241			3.03E-03				
Sr-90		1.31E+04	1.04E+00				
Y-90		1.31E+04	1.04E+00				
Tc-99		3.10E+01	2.54E+02				
Total Curies		5.72E+05	5.44E+06				
Chemicals (kg)							
Ag+			1.31E-06				
Am+3		1.16E-02	2.05E-06				
As+5		1.22E-01	1.17E-06				
B+3		4.13E-02	1.23E-05				
Be+2		4.39E-03	1.75E-05				
Be+2		4.97E-05	1.10E-13				
Bi+3			2.05E-06				
Ca+2		7.36E-02	2.24E-02				
Cd+2		2.70E-03	4.74E-06				
Ce+3		1.11E-01					
Cr+3		1.09E-05					
Co+5		3.44E-05					
Co+		1.26E+01	3.22E+01				
Cr+2		9.57E-03	1.78E-06				
Eu+3			9.16E-08				
Fe+3		2.22E-02	3.22E-02				
Hg+2			2.31E-06				
K+		3.13E+01	1.61E-01				
La+3		8.36E-03	1.75E-04				
Li+		2.07E-02					
Mg+2		3.99E-03	5.05E-05				
Mn+4		2.04E-03	1.10E-02				
Mo+6		6.31E-01	1.42E-05				
Na+		1.71E+04	1.63E+04				
Ni+3		5.85E-03	1.78E-02				
Np+4			2.55E-07				
Pb+4		4.39E-02	7.22E-03				
Pu+4		8.02E-04	2.72E-05				
Re+7		1.03E-02					
Rh+3		7.40E-02					
Ru+3		3.53E-02					
Sb+5		9.57E-02					
Se+6		1.79E-01	8.54E-08				
Si+4		2.60E+00	8.73E-04				

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	11	12	13	14	15	16	17
LIQUID COMPONENTS							
Chemicals (kg) (cont.)							
Sn+4			6.80E-16				
Sn+2			4.53E-01				
Te+6			1.92E-01				
Th+4			1.55E-01				
Ti+4			5.52E-02	8.40E-08			
Ti+3			1.92E+00				
UO2+2			4.26E-01	7.15E-03			
V+5			6.60E-03				
W+6				2.99E-05			
Zn+2			9.82E-03	1.00E-04			
Zn+4				7.63E-07			
Al(OH)4-			5.56E+03	2.70E+00			
Cl-			2.80E+01	1.58E-01			
CO3-2			4.69E+03	4.37E+00			
Cr(OH)4-			2.21E+01	2.94E-02			
F-			2.73E+02	1.08E-01			
I-			1.57E-02				
NO2-			9.52E+03	5.34E+00			
NO3-			1.08E+04	1.58E+01			
OH-			2.25E+03	1.21E+04			
PO4-3			1.80E+00	2.65E-01			
SO4-2			1.01E+00	8.99E-01			
TcO4-			3.02E+00	2.47E+01			
H2O	5.16E+05		1.07E+06	5.57E+03		1.12E+06	
Organic Carbon			1.66E+02	2.55E+00			
ZrO2.2H2O			5.93E-03				
Hg							2.31E-06
Cl2							5.21E+01
CO2							1.31E+04
F2							4.05E+02
I2							2.39E-01
N2							1.47E+03
NO							9.83E+03
NH3							2.96E+01

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	11	12	13	14	15	16	17
SOLID COMPONENTS							
Total Mass Flow (kg)		1.18E+05	9.01E-01	1.81E+05		3.11E+05	

Radionuclides (Ci)							
Am-241		2.50E+04	1.67E+02			2.52E+04	
C-14		1.39E+01					
Om-244		6.41E+02				6.42E+02	
Cs-137		2.15E+05				3.25E+06	
Ba-137						3.12E+06	
Eu-154		2.04E+05				2.42E-02	
Np-237						1.80E-07	
Plu-239		4.84E+02	7.50E+00			4.91E+02	
Plu-240			1.87E+00			1.87E+00	
Plu-241						3.03E-03	
Sr-90		4.64E+06	6.92E+04			4.72E+06	
Y-90		4.64E+06	6.92E+04			4.72E+06	
Tc-99		1.31E+02				4.16E+02	
Total Curies		9.72E+06	1.39E+05			1.59E+07	

Chemicals (kg)							
Al+3		1.04E+04					
Am+3		7.28E+00	4.86E-02				
As+5		1.20E+02					
B+3		6.34E+01					
Be+2		1.56E+02					
Be+2		3.77E+00					
Ca+2		5.23E+02					
Cd+2		1.22E+03					
Ce+3		2.60E+02					
Cr+3		7.91E-03					
Co+3		7.47E-04					
Cr+3		1.70E+02					
Cs+		9.64E+00					
Clp+2		9.27E+01					
Fe+3		2.13E+04					
K+		6.60E+02					
La+3		8.15E+02					
Li+		1.53E+01					
Mg+2		1.31E+02					
Mn+4		6.51E+02					
Mo+6		1.17E+01					
Na+		3.49E+03					
Ni+3		9.53E+02					
Pb+4		1.13E+02					
Plu+4		7.80E+00	1.29E-01				
Re+7		1.22E+01					
Rh+3		9.27E+01					
Ru+3		1.91E+02					
Sb+5		5.85E+02					
Se+6		3.84E+02					
Si+4		1.21E+03					
Sr+2		1.61E+02	4.91E-01				
Te+6		4.12E+02					
Th+4		2.64E+02					
Ti+4		1.42E+02					
Tl+3		1.42E+03					

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	11	12	13	14	15	16	17
SOLID COMPONENTS							
Chemicals (kg) (cont.)							
UO2-2		1.33E+05					
V#5		5.41E+00					
Zn#2		8.67E+01					
Cl-		2.40E+01					
OO3-2		3.28E+03					
F-		1.32E+02					
I-		2.23E-01					
NO2-		1.51E+03					
NO3-		1.24E+03					
OH-		4.90E+04	2.32E-01				
PO4-3		4.99E+01					
SO4-2		5.53E+00					
ToO4-		1.28E+01					
MnO2						1.09E+03	
Organic Carbon		1.80E+03					
ZnO2:2H2O		1.32E+04					
Ag2O						1.41E-06	
Al2O3						2.28E+04	
Am2O3						8.07E+00	
As2O5						1.85E+02	
B2O3				1.54E+04		1.56E+04	
BaO						1.74E+02	
BeO						1.05E+01	
Bi2O3						2.28E-06	
CaO						7.32E+02	
Cd						1.39E+03	
Ce2O3						3.05E+02	
Cr2O3						8.69E-03	
Co2O3						1.10E-03	
Cr2O3						2.62E+02	
Cs2O						5.76E+01	
UO						1.16E+02	
Eu2O3						1.06E-07	
Fe2O3						3.08E+04	
K2O						8.33E+02	
La2O3						9.55E+02	
Li2O				3.08E+03		3.11E+03	
MgO						2.18E+02	
MnO3						1.85E+01	
Nb2O						4.97E+04	
Ni2O3						1.34E+03	
NO2						2.89E-07	
P2O5						3.88E+01	
PbO2						1.31E+02	
PUO2						8.99E+00	
Re2O7						1.59E+01	
Rh2O3						1.14E+02	
Ru2O3						2.36E+02	
Sb2O5						7.77E+02	
SeO3						6.17E+02	
SiO2				1.63E+05		1.65E+05	
SO3						6.20E+00	
SnO						1.91E+02	
Tc2O7						3.88E+01	
TiO3						5.67E+02	
ThO2						3.01E+02	

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Table 10 Phase 1 In-Tank Sludge Washing of DST 241-AZ-101 (10 sheets)

STREAM NAME	11	12	13	14	15	16	17
SOLID COMPONENTS							
Chemicals (kg) (cont.)							
TiO2						2.36E+02	
Ti2O3						1.59E+03	
Li2S						1.41E+03	
V2O5						9.67E+00	
W2S						3.77E+05	
ZrO						1.08E+02	
ZrO2						1.02E+04	

The number of batches resulting from a tank of washed sludge is controlled by the assumed volume of a private contractor receiving tank, and the Specification 8 requirement of no more than 100 g of oxide equivalent of non-volatiles per liter of HLW feed.¹⁰

2.3.2 AZ-102

Figure 11 is the process flow diagram for AZ-102 waste and Table 11 shows the associated mass balance for the retrievable portion of the waste. Stream 1 consists of 95% of the liquids and 60% of the solids in AZ-102. Stream 1 is allowed to self-concentrate to 5M Na (Stream 3). A compacted sludge layer of 50 wt% solids (plus 1 ft of concentrated supernate) remains (Stream 5), after the balance of the supernate is decanted (Stream 4).

Manuel (1996) determined that two washes with two volumes of dilute caustic per volume of settled sludge is appropriate for AZ-102. With transfer solution added back to satisfy Specification 8 (HLW feed slurry parameters), AZ-102 produces two 415,000 L (110,000 gal) batches of HLW feed (Stream 16).

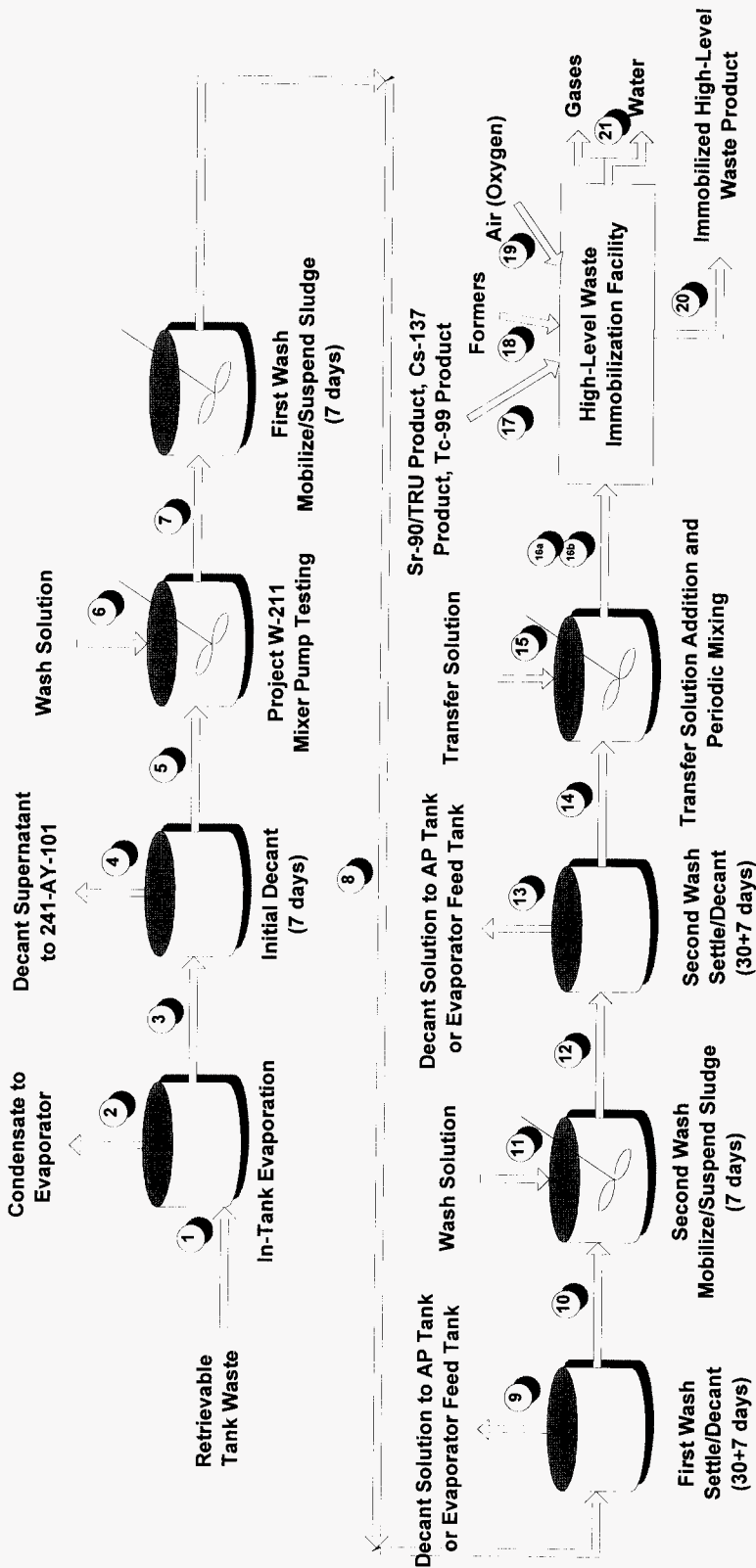
2.3.3 AY-102/C-106

Figure 12 is the process flow diagram for AY-102 and C-106, and Table 12 shows the associated mass balance for the retrievable portion of the waste. Stream 1 consists of 95% of the liquids, 36% of the AY-102 solids, and 99% of the C-106 solids. A compacted sludge layer (64% of AY-102) and a fluffed sludge layer (36% of AY-102 and 99% of C-106), plus 1 ft of supernate, remain (Stream 5) after the balance of the supernate is decanted.

Manuel (1996) determined that two washes with one volume of dilute caustic per volume of settled sludge is appropriate for this blend of sludges. With transfer solution added back to satisfy Specification 8 (HLW feed slurry parameters), AY-102/C-106 produces twelve 430,000 L (113,00 gal) batches of HLW feed (Stream 16).

¹⁰Assumptions have not been made about the private contractor's facility, but assuming the size of the HLW receiving tank is unavoidable. The oxide equivalent limit (100 g/L) for HLW transfers also has ramifications for the number of canisters that result from a batch. The AY/C sludge is higher in sodium than AZ sludge. While AZ sludges produce around 85 canisters per batch, AY/C sludge produces around 45 canisters per batch, because only the non-sodium/non-silicon oxides are counted toward 25 wt% waste loading.

Figure 11. In-Tank Sludge Washing of Double-Shell Tank 241-AZ-102



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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Total Mass Flow (kg)	3.83E+06	1.93E+06	1.90E+06	1.63E+06	2.68E+05	1.44E+06	1.71E+06	1.71E+06	1.13E+06	5.77E+05
Volume (L)	3.45E+06	1.93E+06	1.52E+06	1.30E+06	2.15E+05	1.44E+06	1.65E+06	1.65E+06	1.09E+06	5.57E+05
Specific Gravity	1.11E+00	1.00E+00	1.25E+00	1.25E+00	1.25E+00	1.00E+00	1.04E+00	1.04E+00	1.04E+00	1.04E+00
Radionuclides (Ci)										
Am-241	1.60E+00		1.60E+00	1.37E+00	2.26E-01		2.26E-01	2.26E-01	1.50E-01	7.63E-02
C-14	1.27E+02		1.09E+02	1.09E+02	1.75E+01		1.75E+01	1.75E+01	1.19E+01	6.05E+00
Cs-137	3.02E+06		3.02E+06	2.60E+06	4.27E+05		4.27E+05	4.27E+05	2.83E+05	1.44E+05
Ba-137	2.87E+06		2.87E+06	2.47E+06	4.06E+05		4.06E+05	4.06E+05	2.69E+05	1.37E+05
Eu-154										
Np-237										
Pu-239	3.83E+01		3.83E+01	3.28E+01	5.41E+00		5.41E+00	5.41E+00	3.58E+00	1.83E+00
Pu-240										
Pu-241										
Sr-90	8.49E+03		8.49E+03	7.25E+03	1.20E+03		1.20E+03	1.20E+03	7.95E+02	4.05E+02
Y-90	8.49E+03		8.49E+03	7.25E+03	1.20E+03		1.20E+03	1.20E+03	7.95E+02	4.05E+02
Tc-99	2.86E+02		2.86E+02	2.45E+02	4.04E+01		4.04E+01	4.04E+01	2.68E+01	1.36E+01
Total Curies	5.91E+06		5.91E+06	5.08E+06	8.36E+05		8.36E+05	8.36E+05	5.54E+05	2.82E+05
Chemicals (kg)										
Ag+										
Am#3	4.66E-04		4.66E-04	4.00E-04	6.58E-05		6.58E-05	6.58E-05	4.36E-05	2.22E-05
As#5	3.94E+00		3.94E+00	3.39E+00	5.57E-01		5.57E-01	5.57E-01	3.69E-01	1.88E-01
B#3	2.19E+00		2.19E+00	1.88E+00	3.09E-01		3.09E-01	3.09E-01	2.05E-01	1.04E-01
Be#2	3.05E-01		3.05E-01	2.62E-01	4.31E-02		4.31E-02	4.31E-02	2.86E-02	1.46E-02
Be#2	2.01E-02		2.01E-02	1.73E-02	2.85E-03		2.85E-03	2.85E-03	1.89E-03	9.61E-04
Bi#3										
Ca#2	1.06E+01		1.06E+01	9.13E+00	1.50E+00		1.50E+00	1.50E+00	9.95E-01	5.07E-01
Ca#2	3.43E-01		3.43E-01	2.95E-01	4.85E-02		4.85E-02	4.85E-02	3.21E-02	1.64E-02
Ca#3	3.87E+00		3.87E+00	3.32E+00	5.47E-01		5.47E-01	5.47E-01	3.62E-01	1.85E-01
Co#3	3.55E-05		3.55E-05	3.05E-05	5.02E-06		5.02E-06	5.02E-06	3.33E-06	1.70E-06
Co#	1.36E+02		1.36E+02	1.17E+02	1.92E+01		1.92E+01	1.92E+01	1.27E+01	6.49E+00
Cr#2	2.75E-01		2.75E-01	2.40E-01	3.95E-02		3.95E-02	3.95E-02	2.61E-02	1.33E-02
Eu#3										
Fe#3	2.89E+00		2.89E+00	2.49E+00	4.09E-01		4.09E-01	4.09E-01	2.71E-01	1.38E-01
Hg#2										
K#	2.48E+02		2.48E+02	2.13E+02	3.51E+01		3.51E+01	3.51E+01	2.32E+01	1.18E+01
La#3	6.20E-01		6.20E-01	5.33E-01	8.77E-02		8.77E-02	8.77E-02	5.81E-02	2.96E-02
Li#	2.80E-01		2.80E-01	2.40E-01	3.96E-02		3.96E-02	3.96E-02	2.62E-02	1.34E-02
Mg#2	3.50E-01		3.50E-01	3.01E-01	4.95E-02		4.95E-02	4.95E-02	3.28E-02	1.67E-02
Mn#4	2.64E-01		2.64E-01	2.26E-01	3.73E-02		3.73E-02	3.73E-02	2.47E-02	1.26E-02
Mo#6	6.41E+00		6.41E+00	5.51E+00	9.05E-01		9.05E-01	9.05E-01	6.00E-01	3.06E-01
Na#	1.75E+05		1.75E+05	1.50E+05	2.47E+04	3.63E+03	2.83E+04	2.83E+04	1.89E+04	9.54E+03
Ni#3	6.67E-01		6.67E-01	5.73E-01	9.43E-02		9.43E-02	9.43E-02	6.25E-02	3.18E-02
Np#4										
Pb#4	1.37E+00		1.37E+00	1.17E+00	1.93E-01		1.93E-01	1.93E-01	1.28E-01	6.52E-02
Pu#4	6.17E-01		6.17E-01	5.30E-01	8.72E-02		8.72E-02	8.72E-02	5.78E-02	2.95E-02
Re#7	2.08E-01		2.08E-01	1.75E-01	2.94E-02		2.94E-02	2.94E-02	1.95E-02	9.94E-03
Rh#3	2.66E+00		2.66E+00	2.29E+00	3.76E-01		3.76E-01	3.76E-01	2.49E-01	1.27E-01
Ru#3	6.60E-01		6.60E-01	5.67E-01	9.33E-02		9.33E-02	9.33E-02	6.18E-02	3.15E-02
Se#6	3.24E+00		3.24E+00	2.78E+00	4.58E-01		4.58E-01	4.58E-01	3.03E-01	1.55E-01
Si#4	1.71E+03		1.71E+03	1.47E+03	2.42E+02		2.42E+02	2.42E+02	1.60E+02	8.17E+01
Si#4										
Sm#2	8.70E-01		8.70E-01	7.47E-01	1.23E-01		1.23E-01	1.23E-01	8.14E-02	4.15E-02
Te#6	8.24E-01		8.24E-01	7.08E-01	1.17E-01		1.17E-01	1.17E-01	7.72E-02	3.94E-02

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Chemicals (kg) (cont.)										
Ti+4	2.32E-01		2.32E-01	2.00E-01	3.29E-02		3.29E-02	3.29E-02	2.18E-02	1.11E-02
Ti+3	5.69E-01		5.69E-01	4.88E-01	8.04E-02		8.04E-02	8.04E-02	5.32E-02	2.71E-02
UO2+2	5.48E+03		5.48E+03	4.70E+03	7.74E+02		7.74E+02	7.74E+02	5.13E+02	2.62E+02
V+5	2.45E-01		2.45E-01	2.10E-01	3.46E-02		3.46E-02	3.46E-02	2.29E-02	1.17E-02
W+6										
Zn+2	1.32E-01		1.32E-01	1.14E-01	1.87E-02		1.87E-02	1.87E-02	1.24E-02	6.31E-03
Zn+4										
Al(OH)+-	1.69E+04		1.69E+04	1.45E+04	2.38E+03		2.38E+03	2.38E+03	1.58E+03	8.04E+02
Cl-										
CO3-2	8.99E+04		8.99E+04	7.72E+04	1.27E+04		1.27E+04	1.27E+04	8.41E+03	4.29E+03
Cr(OH)+-	7.27E+03		7.27E+03	6.24E+03	1.03E+03		1.03E+03	1.03E+03	6.80E+02	3.47E+02
F-	3.18E+03		3.18E+03	2.73E+03	4.50E+02		4.50E+02	4.50E+02	2.98E+02	1.52E+02
I-	8.13E-02		8.13E-02	6.98E-02	1.15E-02		1.15E-02	1.15E-02	7.61E-03	3.89E-03
NO2-	8.81E+04		8.81E+04	7.57E+04	1.25E+04	6.60E+02	1.31E+04	1.31E+04	8.69E+03	4.43E+03
NO3-	7.34E+04		7.34E+04	6.30E+04	1.04E+04		1.04E+04	1.04E+04	6.87E+03	3.50E+03
OH-	5.14E+04		5.14E+04	4.41E+04	7.27E+02	2.44E+03	3.17E+03	3.17E+03	2.10E+03	1.07E+03
PO4-3	3.14E+01		3.14E+01	2.69E+01	4.43E+00		4.43E+00	4.43E+00	2.94E+00	1.50E+00
SO4-2	5.31E+04		5.31E+04	4.56E+04	7.51E+03		7.51E+03	7.51E+03	4.98E+03	2.54E+03
ToO4-	2.78E+01		2.78E+01	2.39E+01	3.93E+00		3.93E+00	3.93E+00	2.61E+00	1.33E+00
H2O	3.31E+06	1.93E+06	1.39E+06	1.18E+06	1.94E+05	1.43E+06	1.63E+06	1.63E+06	1.08E+06	5.50E+05
Organic Carbon	4.72E+03		4.72E+03	4.05E+03	6.67E+02		6.67E+02	6.67E+02	4.42E+02	2.25E+02
ZrO2:2H2O	1.12E+00		1.12E+00	9.64E-01	1.59E-01		1.59E-01	1.59E-01	1.05E-01	5.36E-02
Hg										
Cl2										
CO2										
F2										
I2										
N2										
NO										
O2										
NH3										

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	1.13E+05		1.13E+05	3.72E+02	1.12E+05		1.12E+05	1.12E+05	3.70E+02	1.12E+05
Radionuclides (Ci)										
Am-241	1.01E+04		1.01E+04	3.33E+01	1.00E+04		1.00E+04	1.00E+04	3.31E+01	1.00E+04
C-14	7.48E+00		7.48E+00	2.47E-02	7.45E+00		7.45E+00	7.45E+00	2.46E-02	7.43E+00
Om-244	3.25E+02		3.25E+02	1.07E+00	3.24E+02		3.24E+02	3.24E+02	1.07E+00	3.23E+02
Cs-137	1.73E+05		1.73E+05	5.70E+02	1.72E+05		1.72E+05	1.72E+05	5.69E+02	1.72E+05
Ba-137	1.64E+05		1.64E+05	5.42E+02	1.64E+05		1.64E+05	1.64E+05	5.40E+02	1.63E+05
Eu-154										
Np-237										
Plu-239	2.89E+02		2.89E+02	9.55E-01	2.88E+02		2.88E+02	2.88E+02	9.51E-01	2.87E+02
Plu-240										
Plu-241										
Sr-90	1.78E+06		1.78E+06	5.87E+03	1.77E+06		1.77E+06	1.77E+06	5.85E+03	1.77E+06
Y-90	1.78E+06		1.78E+06	5.87E+03	1.77E+06		1.77E+06	1.77E+06	5.85E+03	1.77E+06
Tc-99	8.83E+01		8.83E+01	2.91E-01	8.80E+01		8.80E+01	8.80E+01	2.90E-01	8.77E+01
Total Curies	3.91E+06		3.91E+06	1.25E+04	3.89E+06		3.89E+06	3.89E+06	1.28E+04	3.88E+06
Chemicals (kg)										
Al+3	9.25E+03		9.25E+03	3.05E+01	9.21E+03		9.21E+03	9.21E+03	3.04E+01	9.18E+03
Am#3	2.94E+00		2.94E+00	9.69E-03	2.93E+00		2.93E+00	2.93E+00	9.66E-03	2.92E+00
As+5	9.94E+01		9.94E+01	3.28E-01	9.90E+01		9.90E+01	9.90E+01	3.27E-01	9.87E+01
B#3	8.34E+01		8.34E+01	2.75E-01	8.31E+01		8.31E+01	8.31E+01	2.74E-01	8.28E+01
Be#2	9.50E+01		9.50E+01	3.14E-01	9.47E+01		9.47E+01	9.47E+01	3.13E-01	9.44E+01
Be#2	2.31E+00		2.31E+00	7.61E-03	2.30E+00		2.30E+00	2.30E+00	7.59E-03	2.29E+00
Ca#2	4.86E+02		4.86E+02	1.61E+00	4.85E+02		4.85E+02	4.85E+02	1.60E+00	4.83E+02
Ca#2	2.59E+03		2.59E+03	8.55E+00	2.58E+03		2.58E+03	2.58E+03	8.53E+00	2.58E+03
Ca#3	1.33E+02		1.33E+02	4.39E-01	1.33E+02		1.33E+02	1.33E+02	4.38E-01	1.32E+02
Cl#3	4.01E-03		4.01E-03	1.32E-05	4.00E-03		4.00E-03	4.00E-03	1.32E-05	3.98E-03
Co#3	3.21E-05		3.21E-05	1.06E-07	3.20E-05		3.20E-05	3.20E-05	1.06E-07	3.19E-05
Cr+3	2.17E+02		2.17E+02	7.16E-01	2.16E+02		2.16E+02	2.16E+02	7.13E-01	2.15E+02
Cs#	7.74E+00		7.74E+00	2.56E-02	7.72E+00		7.72E+00	7.72E+00	2.55E-02	7.69E+00
Clu#2	6.00E+01		6.00E+01	1.98E-01	5.98E+01		5.98E+01	5.98E+01	1.97E-01	5.96E+01
Fe#3	2.26E+04		2.26E+04	7.47E+01	2.26E+04		2.26E+04	2.26E+04	7.45E+01	2.25E+04
K#	2.02E+02		2.02E+02	6.67E-01	2.02E+02		2.02E+02	2.02E+02	6.66E-01	2.01E+02
La#3	7.74E+02		7.74E+02	2.56E+00	7.72E+02		7.72E+02	7.72E+02	2.55E+00	7.69E+02
Li#	4.84E+00		4.84E+00	1.63E-02	4.82E+00		4.82E+00	4.82E+00	1.62E-02	4.81E+00
Mg#2	1.64E+02		1.64E+02	5.42E-01	1.64E+02		1.64E+02	1.64E+02	5.40E-01	1.63E+02
Mn#6	4.98E+02		4.98E+02	1.64E+00	4.96E+02		4.96E+02	4.96E+02	1.64E+00	4.94E+02
Mo#6	4.05E+00		4.05E+00	1.34E-02	4.04E+00		4.04E+00	4.04E+00	1.33E-02	4.03E+00
Na#	7.14E+03		7.14E+03	2.36E+01	7.11E+03		7.11E+03	7.11E+03	2.35E+01	7.09E+03
Ni+3	1.53E+03		1.53E+03	5.05E+00	1.52E+03		1.52E+03	1.52E+03	5.03E+00	1.52E+03
Pb#4	1.89E+02		1.89E+02	6.24E-01	1.89E+02		1.89E+02	1.89E+02	6.22E-01	1.88E+02
Plu#4	4.67E+00		4.67E+00	1.54E-02	4.65E+00		4.65E+00	4.65E+00	1.54E-02	4.64E+00
Re#7	1.24E+01		1.24E+01	4.08E-02	1.23E+01		1.23E+01	1.23E+01	4.06E-02	1.22E+01
Rh+3	7.14E+01		7.14E+01	2.36E-01	7.11E+01		7.11E+01	7.11E+01	2.35E-01	7.09E+01
Ru+3	3.09E+01		3.09E+01	1.02E-01	3.08E+01		3.08E+01	3.08E+01	1.02E-01	3.07E+01
Se#6	1.75E+02		1.75E+02	5.75E-01	1.75E+02		1.75E+02	1.75E+02	5.77E-01	1.74E+02
Si#4	7.26E+02		7.26E+02	2.40E+00	7.23E+02		7.23E+02	7.23E+02	2.39E+00	7.21E+02
Sr+2	7.00E+01		7.00E+01	2.31E-01	6.98E+01		6.98E+01	6.98E+01	2.30E-01	6.95E+01
Te#6	5.90E+01		5.90E+01	1.95E-01	5.88E+01		5.88E+01	5.88E+01	1.94E-01	5.86E+01
Ti#4	1.32E+01		1.32E+01	4.36E-02	1.32E+01		1.32E+01	1.32E+01	4.35E-02	1.31E+01
Tl+3	9.50E+00		9.50E+00	3.14E-02	9.47E+00		9.47E+00	9.47E+00	3.13E-02	9.44E+00
UO2#2	2.37E+03		2.37E+03	7.81E+00	2.36E+03		2.36E+03	2.36E+03	7.79E+00	2.35E+03
V#5	5.49E+00		5.49E+00	1.81E-02	5.47E+00		5.47E+00	5.47E+00	1.81E-02	5.45E+00
Zn#2	2.43E+01		2.43E+01	8.01E-02	2.42E+01		2.42E+01	2.42E+01	7.99E-02	2.41E+01

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Chemicals (kg) (cont.)										
Cl-	2.54E+01		2.54E+01	8.39E-02	2.53E+01		2.53E+01	2.53E+01	8.36E-02	2.52E+01
Cl3-2	1.35E+04		1.35E+04	4.45E+01	1.34E+04		1.34E+04	1.34E+04	4.43E+01	1.34E+04
F-	2.14E+01		2.14E+01	7.07E-02	2.14E+01		2.14E+01	2.14E+01	7.05E-02	2.13E+01
I-	1.43E-01		1.43E-01	4.73E-04	1.43E-01		1.43E-01	1.43E-01	4.72E-04	1.43E-01
NO2-	6.54E+02		6.54E+02	2.16E+00	6.52E+02		6.52E+02	6.52E+02	2.15E+00	6.50E+02
NO3-	1.81E+02		1.81E+02	5.99E-01	1.81E+02		1.81E+02	1.81E+02	5.97E-01	1.80E+02
OH-	4.25E+04		4.25E+04	1.40E+02	4.24E+04		4.24E+04	4.24E+04	1.40E+02	4.22E+04
PO4-3	5.20E+01		5.20E+01	1.72E-01	5.18E+01		5.18E+01	5.18E+01	1.71E-01	5.17E+01
SO4-2	2.37E+00		2.37E+00	7.81E-03	2.36E+00		2.36E+00	2.36E+00	7.79E-03	2.35E+00
TcO4-	8.60E+00		8.60E+00	2.84E-02	8.57E+00		8.57E+00	8.57E+00	2.83E-02	8.54E+00
MnO2										
Organic Carbon	4.74E+02		4.74E+02	1.57E+00	4.73E+02		4.73E+02	4.73E+02	1.56E+00	4.71E+02
ZrO2.2H2O	5.47E+03		5.47E+03	1.81E+01	5.45E+03		5.45E+03	5.45E+03	1.80E+01	5.43E+03
Ag2O										
Al2O3										
Am2O3										
As2O3										
B2O3										
BaO										
BaO										
Bi2O3										
CaO										
CaO										
Ca2O3										
Cr2O3										
Co2O3										
Cr2O3										
Cs2O										
UO										
Ba2O3										
Fe2O3										
K2O										
La2O3										
Li2O										
MgO										
MgO										
MoO3										
Na2O										
NI2O3										
NI2O3										
P2O5										
PbO2										
PlO2										
Re2O7										
Rh2O3										
Ru2O3										
SeO3										
SiO2										
SO3										
SiO										
Tc2O7										
TcO3										
TiO2										
Ti2O3										
UO3										
V2O5										
WCl3										
ZnO										
ZrO2										

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Total Mass Flow (kg)	1.44E+06	2.02E+06	1.44E+06	5.72E+05	2.65E+05	8.37E+05	2.55E+04		3.93E+02	
Volume (L)	1.44E+06	1.99E+06	1.43E+06	5.66E+05	2.65E+05	8.30E+05	1.06E+04		3.93E+02	
Specific Gravity	1.00E+00	1.01E+00	1.01E+00	1.01E+00	1.00E+00	1.01E+00	2.41E+00		1.00E+00	
Radionuclides (Ci)										
Am-241		7.63E-02	5.46E-02	2.17E-02		2.17E-02	5.31E-03			
C-14		6.09E+00	4.34E+00	1.72E+00		1.72E+00	3.06E-04			
Cs-137		1.44E+05	1.03E+05	4.10E+04		4.10E+04	2.10E+06			
Ba-137		1.37E+05	9.82E+04	3.89E+04		3.89E+04	1.99E+06			
Eu-154							1.81E-02			
Np-237							1.35E-07			
Pu-239		1.83E+00	1.31E+00	5.18E-01		5.18E-01	1.18E-03			
Pu-240							2.94E-04			
Pu-241							2.27E-03			
Sr-90		4.05E+02	2.90E+02	1.15E+02		1.15E+02	7.79E-01			
Y-90		4.05E+02	2.90E+02	1.15E+02		1.15E+02	1.79E-01			
Tc-99		1.36E+01	9.77E+00	3.87E+00		3.87E+00	7.00E+02			
Total Curies		2.82E+05	2.02E+05	8.01E+04		8.01E+04	4.09E+06			
Chemicals (kg)										
Ag+							9.85E-07			
Am+3		2.22E-05	1.59E-05	6.31E-06		6.31E-06	1.55E-06			
As+5		1.89E-01	1.35E-01	5.34E-02		5.34E-02	8.73E-07			
B+3		1.04E-01	7.47E-02	2.96E-02		2.96E-02	9.25E-07			
Ba+2		1.46E-02	1.04E-02	4.13E-03		4.13E-03	1.31E-05			
Be+2		9.61E-04	6.89E-04	2.73E-04		2.73E-04	8.26E-14			
Bi+3							1.54E-06			
Ca+2		5.07E-01	3.63E-01	1.44E-01		1.44E-01	1.68E-02			
Ca+2		1.64E-02	1.17E-02	4.65E-03		4.65E-03	3.56E-06			
Ca+3		1.85E-01	1.32E-01	5.25E-02		5.25E-02				
Co+3		1.70E-06	1.21E-06	4.81E-07		4.81E-07				
Co+		6.49E+00	4.65E+00	1.84E+00		1.84E+00	2.42E+01			
Cr+2		1.33E-02	9.54E-03	3.78E-03		3.78E-03	1.34E-06			
Eu+3							6.84E-08			
Fe+3		1.39E-01	9.90E-02	3.92E-02		3.92E-02	2.46E-02			
Hg+2							1.73E-06			
K+		1.18E+01	8.48E+00	3.36E+00		3.36E+00	1.21E-01			
La+3		2.94E-02	2.12E-02	8.41E-03		8.41E-03	1.31E-04			
Li+		1.34E-02	9.57E-03	3.79E-03		3.79E-03				
Mg+2		1.67E-02	1.20E-02	4.74E-03		4.74E-03	3.80E-05			
Mn+4		1.26E-02	9.01E-03	3.57E-03		3.57E-03	8.20E-03			
Mo+6		3.05E-01	2.19E-01	8.69E-02		8.69E-02	1.06E-05			
Nb+		1.32E+04	9.44E+03	3.74E+03		3.74E+03	1.22E+04			
Ni+3		3.18E-02	2.29E-02	9.04E-03		9.04E-03	1.33E-02			
Ni+4							1.91E-07			
Pb+4		6.52E-02	4.67E-02	1.85E-02		1.85E-02	5.42E-03			
Pu+4		2.95E-02	2.11E-02	8.34E-03		8.34E-03	2.04E-05			
Re+7		9.94E-03	7.12E-03	2.82E-03		2.82E-03				
Rh+3		1.27E-01	9.10E-02	3.61E-02		3.61E-02				
Ru+3		3.15E-02	2.26E-02	8.95E-03		8.95E-03				
Se+6		1.55E-01	1.11E-01	4.39E-02		4.39E-02	6.40E-08			
Si+4		8.17E+01	5.85E+01	2.32E+01		2.32E+01	6.54E-04			
Sn+4							5.10E-16			
Sn+2		4.15E-02	2.97E-02	1.18E-02		1.18E-02	5.52E-06			
Te+6		3.94E-02	2.82E-02	1.12E-02		1.12E-02				
Ti+4		1.11E-02	7.95E-03	3.15E-03		3.15E-03	6.30E-08			

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Chemicals (kg) (cont.)										
TI+3		2.71E-02	1.94E-02	7.71E-03		7.71E-03				
UO2+2		2.62E+02	1.67E+02	7.42E+01		7.42E+01				
W5		1.17E-02	8.36E-03	3.31E-03		3.31E-03		5.36E-03		
W6								2.24E-05		
Zn+2		6.31E-03	4.52E-03	1.79E-03		1.79E-03		7.50E-05		
Zn+4								5.72E-07		
Al(OH)4-		8.04E+02	5.76E+02	2.28E+02		2.28E+02		2.02E+00		
Cl-								1.18E-01		
CO3-2		4.29E+03	3.07E+03	1.22E+03		1.22E+03		3.28E+00		
Cr(OH)4-		3.47E+02	2.48E+02	9.85E+01		9.85E+01		2.20E-02		
F-		1.52E+02	1.09E+02	4.31E+01		4.31E+01		8.08E-02		
I-		3.88E-03	2.78E-03	1.10E-03		1.10E-03				
NO2-	6.60E+02	5.09E+03	3.65E+03	1.45E+03		1.45E+03		4.02E+00		
NO3-		3.50E+03	2.51E+03	9.94E+02		9.94E+02		1.18E+01		
OH-	2.44E+03	3.51E+03	2.51E+03	9.96E+02		9.96E+02		9.03E+03		
PO4-3		1.50E+00	1.07E+00	4.25E-01		4.25E-01		1.99E-01		
SO4-2		2.54E+03	1.82E+03	7.23E+02		7.23E+02		6.74E-01		
TCO4-		1.33E+00	9.51E-01	3.77E-01		3.77E-01		1.85E+01		
H2O	1.43E+06	1.98E+06	1.42E+06	5.63E+05	2.65E+05	5.63E+05		4.18E+03		
Organic Carbon		2.25E+02	1.61E+02	6.39E+01		6.39E+01		1.92E+00		
ZrO2·2H2O		5.36E-02	3.84E-02	1.52E-02		1.52E-02				
Hg										
Cl2										
CO2										
F2										
I2										
N2										
NO										
O2										
NH3								3.93E+02		

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Total Mass Flow (kg)		1.12E+05	3.69E+02	1.12E+05		1.12E+05	6.75E-01	1.68E+05		2.67E+05
Radionuclides (Ci)										
Am-241		1.00E+04	3.30E+01	9.98E+03		9.98E+03	1.25E+02			1.01E+04
C-14		7.43E+00	2.45E-02	7.40E+00		7.40E+00				7.40E+00
Cr-244		3.22E+02	1.07E+00	3.22E+02		3.22E+02				3.22E+02
Cs-137		1.72E+05	5.67E+02	1.71E+05		1.71E+05				2.31E+05
Ba-137		1.63E+05	5.38E+02	1.63E+05		1.63E+05				2.19E+05
Eu-154										1.81E-02
Np-237										1.35E-07
Pu-239		2.87E+02	9.48E-01	2.86E+02		2.86E+02	5.63E+00			2.93E+02
Pu-240							1.40E+00			1.40E+00
Pu-241										2.27E-03
Si-90		1.77E+06	5.83E+03	1.76E+06		1.76E+06	5.19E+04			1.81E+06
Y-90		1.77E+06	5.83E+03	1.76E+06		1.76E+06	5.19E+04			1.81E+06
Tc-99		8.77E+01	2.90E-01	8.74E+01		8.74E+01				2.82E-02
Total Curies		3.88E+06	1.28E+04	3.87E+06		3.87E+06	1.04E+05			8.14E+06
Chemicals (kg)										
Al+3		9.18E+03	3.03E+01	9.15E+03		9.15E+03				
Am+3		2.92E+00	9.63E-03	2.91E+00		2.91E+00	3.64E-02			
As+5		9.87E+01	3.26E-01	9.84E+01		9.84E+01				
B+3		8.28E+01	2.73E-01	8.26E+01		8.26E+01				
Ba+2		9.44E+01	3.12E-01	9.41E+01		9.41E+01				
Be+2		2.29E+00	7.56E-03	2.28E+00		2.28E+00				
Ca+2		4.83E+02	1.60E+00	4.82E+02		4.82E+02				
Ca+2		2.58E+03	8.50E+00	2.57E+03		2.57E+03				
Ce+3		1.32E+02	4.36E-01	1.32E+02		1.32E+02				
Cr+3		3.98E-03	1.31E-05	3.97E-03		3.97E-03				
Co+3		3.19E-05	1.05E-07	3.18E-05		3.18E-05				
Cr+3		2.15E+02	7.11E-01	2.15E+02		2.15E+02				
Dst		7.69E+00	2.54E-02	7.67E+00		7.67E+00				
Dst+2		5.98E+01	1.97E-01	5.94E+01		5.94E+01				
Fe+3		2.25E+04	7.42E+01	2.24E+04		2.24E+04				
K+		2.01E+02	6.63E-01	2.00E+02		2.00E+02				
Li+3		7.69E+02	2.54E+00	7.67E+02		7.67E+02				
Li+		4.81E+00	1.59E-02	4.79E+00		4.79E+00				
Mg+2		1.63E+02	5.38E-01	1.63E+02		1.63E+02				
Mn+4		4.94E+02	1.63E+00	4.93E+02		4.93E+02				
Mo+6		4.03E+00	1.33E-02	4.01E+00		4.01E+00				
Nb+		7.09E+03	2.34E+01	7.07E+03		7.07E+03				
Ni+3		1.52E+03	5.01E+00	1.51E+03		1.51E+03				
Pb+4		1.88E+02	6.20E-01	1.87E+02		1.87E+02				
Pu+4		4.64E+00	1.53E-02	4.62E+00		4.62E+00	9.69E-02			
Re+7		1.23E+01	4.05E-02	1.22E+01		1.22E+01				
Rh+3		7.09E+01	2.34E-01	7.07E+01		7.07E+01				
Ru+3		3.07E+01	1.01E-01	3.06E+01		3.06E+01				
Se+6		1.74E+02	5.75E-01	1.74E+02		1.74E+02				
Si+4		7.21E+02	2.38E+00	7.19E+02		7.19E+02				
Si+2		6.95E+01	2.25E-01	6.93E+01		6.93E+01	3.68E-01			
Te+6		5.88E+01	1.94E-01	5.84E+01		5.84E+01				
Ti+4		1.31E+01	4.33E-02	1.31E+01		1.31E+01				
Ti+3		9.44E+00	3.12E-02	9.41E+00		9.41E+00				
UO2+2		2.35E+03	7.76E+00	2.34E+03		2.34E+03				
V+5		5.45E+00	1.80E-02	5.43E+00		5.43E+00				
Zn+2		2.41E+01	7.98E-02	2.40E+01		2.40E+01				

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Chemicals (kg) (cont.)										
Cl-		2.52E+01	8.33E-02	2.52E+01		2.52E+01				
Cl2		1.34E+04	4.42E+01	1.34E+04		1.34E+04				
F-		2.13E+01	7.02E-02	2.12E+01		2.12E+01				
I-		1.42E-01	4.70E-04	1.42E-01		1.42E-01				
NO2-		6.50E+02	2.14E+00	6.48E+02		6.48E+02				
NO3-		1.80E+02	5.95E-01	1.80E+02		1.80E+02				
OH-		4.22E+04	1.39E+02	4.21E+04		4.21E+04	1.74E-01			
PO4-3		5.17E+01	1.71E-01	5.15E+01		5.15E+01				
SO4-2		2.35E+00	7.78E-03	2.34E+00		2.34E+00				
Tox4-Mn02		8.54E+00	2.82E-02	8.51E+00		8.51E+00				7.80E+02
Organic Carbon		4.71E+02	1.56E+00	4.70E+02		4.70E+02				
Zr02:2H2O		5.43E+03	1.79E+01	5.42E+03		5.42E+03				
Ag2O										1.06E-06
Al2O3										1.74E+04
Am2O3										3.24E+00
As2O3										1.51E+02
B2O3								1.44E+04		1.47E+04
BaO										1.05E+02
BeO										6.34E+00
Bi2O3										1.72E-06
CaO										6.74E+02
CaD										2.93E+03
Ce2O3										1.54E+02
Cr2O3										4.36E-03
Co2O3										4.55E-05
Cr2O3										3.76E+02
Cs2O										3.57E+01
UO										7.43E+01
Eu2O3										7.92E-08
Fe2O3										3.21E+04
K2O										2.45E+02
La2O3										8.99E+02
Li2O								2.66E+03		2.67E+03
MgO										2.70E+02
MoO3										6.15E+00
Na2O										3.10E+04
Ni2O3										2.13E+03
NO2										2.17E-07
NO3										3.53E+01
P2O5										2.16E+02
PbO2										5.34E+00
PlO2										1.59E+01
Re2O7										8.72E+01
Rh2O3										3.79E+01
Ru2O3										2.79E+02
SeO3										1.52E+05
SiO2								1.51E+05		6.03E+02
SO3										8.21E+01
SiO										2.61E+01
Tc2O7										8.04E+01
TaO3										2.18E+01
TiO2										1.05E+01
Tl2O3										2.56E+03
UO3										9.70E+00
V2O5										2.82E-05
WO3										2.99E+01
ZnO										4.19E+03
ZrO2										

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME		21
LIQUID COMPONENTS		
Total Mass Flow (kg)		8.75E+05
Volume (L)		8.75E+05
Specific Gravity		1.00E+00

Radionuclides (Ci)	
Am-241	
C-14	
Cs-137	
Ba-137	
Eu-154	
Np-237	
Pu-239	
Pu-240	
Pu-241	
Sr-90	
Y-90	
Tc-99	
Total Curies	

Chemicals (kg)	
Ag+	
Am+3	
As+5	
B+3	
Ba+2	
Be+2	
Bi+3	
Ca+2	
Cd+2	
Ce+3	
Co+3	
Cs+	
Cr+2	
Eu+3	
Fe+3	
Hg+2	
K+	
La+3	
Li+	
Mg+2	
Mn+4	
Mo+6	
Na+	
Ni+3	
Nb+4	
Pb+4	
Pu+4	
Re+7	
Rh+3	
Ru+3	
Se+6	
Si+4	
Sn+4	
Sr+2	
Te+6	
Ti+4	

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	21
LIQUID COMPONENTS	
Chemicals (kg) (cont.)	
Ti+3	
Li2+2	
W+6	
W+6	
Zn+2	
Zn+4	
Al(OH)+3	
Cl-	
CO3-2	
Cr(OH)+3	
F-	
I-	
NO2-	
NO3-	
OH-	
PO4-3	
SO4-2	
TcO4-	
H2O	8.60E+05
Organic Carbon	
ZrO2·2H2O	
Hg	1.73E-06
Cl2	2.53E+01
CO2	1.26E+04
F2	6.44E+01
I2	1.43E+01
N2	2.19E+02
NO	1.46E+03
O2	
NH3	4.41E+00

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	Z1
SOLID COMPONENTS	
Total Mass Flow (kg)	

Radionuclides (Ci)	
Am-241	
C-14	
Om-244	
Cs-137	
Ba-137	
Eu-154	
Np-237	
Plu-239	
Plu-240	
Plu-241	
Sr-90	
Y-90	
Tc-99	
Total Curies	

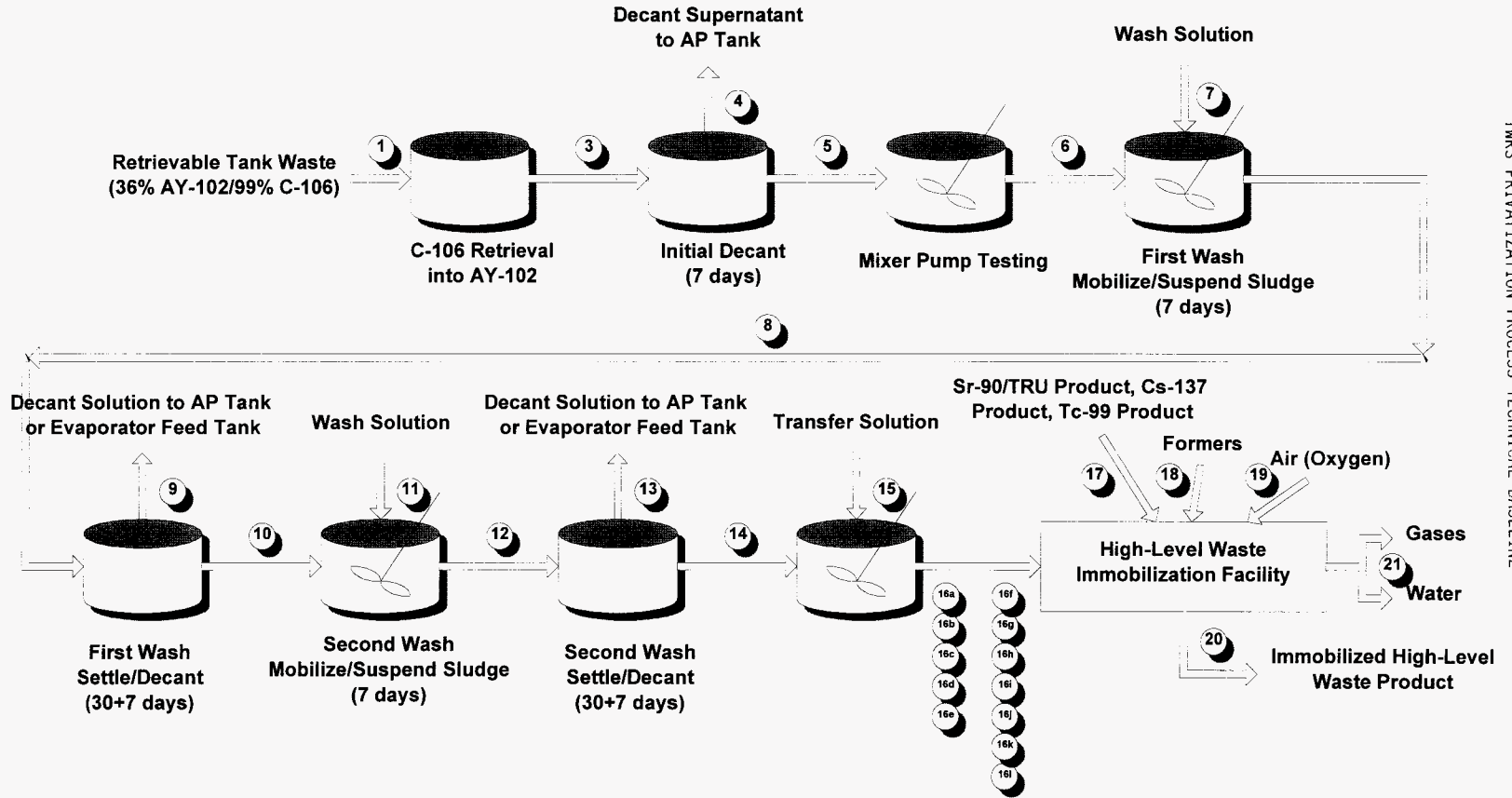
Chemicals (kg)	
Al+3	
Am+3	
As+5	
B+3	
Be+2	
Be+2	
Ca+2	
Ca+2	
Ce+3	
Co+3	
Co+3	
Cr+3	
Cs+	
Du+2	
Fe+3	
K+	
La+3	
Li+	
Mg+2	
Mn+6	
Mo+6	
Na+	
Ni+3	
Pb+4	
Plu+4	
Re+7	
Rh+3	
Ru+3	
Se+6	
Si+4	
Sr+2	
Te+6	
Ti+4	
Tl+3	
UO2+2	
V+5	
Zn+2	

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Table 11 Phase 1 In-Tank Sludge Washing of DST 241-AZ-102 (60% Retrieval) (12 sheets)

STREAM NAME	21
SOLID COMPONENTS	
Chemicals (kg) (cont.)	
Cl-	
CO3-2	
F-	
I-	
NO2-	
NO3-	
OH-	
PO4-3	
SO4-2	
To4-	
MnO2	
Organic Carbon	
ZrO2·2H2O	
Ag2O	
Al2O3	
Am2O3	
As2O3	
B2O3	
BaO	
BaO	
Bi2O3	
CaO	
CaO	
Ca2O3	
Cr2O3	
Co2O3	
Cr2O3	
Cs2O	
ClO	
Eu2O3	
Fe2O3	
K2O	
La2O3	
Li2O	
MgO	
MnO3	
Na2O	
Ni2O3	
NiO2	
P2O5	
PrO2	
PlO2	
Re2O7	
Rh2O3	
Ru2O3	
SeO3	
SiO2	
SO3	
SiO	
Tc2O7	
TaO3	
TiO2	
Ti2O3	
UO3	
V2O5	
WO3	
ZnO	
ZnO2	

Figure 12. In-Tank Sludge Washing of Double-Shell Tank 241-AY-102/SST 241-C-106



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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/SST 241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Total Mass Flow (kg)	3.90E+06		3.90E+06	2.46E+06	1.44E+06	1.44E+06	1.45E+06	2.89E+06	1.45E+06	1.43E+06
Volume (L)	3.87E+06		3.87E+06	2.44E+06	1.43E+06	1.43E+06	1.44E+06	2.87E+06	1.43E+06	1.43E+06
Specific Gravity	1.01E+00		1.01E+00	1.01E+00	1.01E+00	1.01E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00

Radionuclides (Ci)										
Atr-241	1.55E+01		1.55E+01	9.78E+00	5.72E+00	5.72E+00		5.72E+00	2.88E+00	2.84E+00
C-14										
Om-244	1.34E-02		1.34E-02	8.48E-03	4.96E-03	4.96E-03		4.96E-03	2.50E-03	2.42E-03
Co-60	4.57E+00		2.88E+00	1.69E+00	1.69E+00	1.69E+00		1.69E+00	8.49E-01	8.39E-01
Cs-137	6.86E+04		6.86E+04	4.33E+04	2.53E+04	2.53E+04		2.53E+04	1.28E+04	1.26E+04
Ba-137	6.52E+04		6.52E+04	4.11E+04	2.41E+04	2.41E+04		2.41E+04	1.21E+04	1.20E+04
Eu-154										
Np-237										
Pu-239	1.54E+02		1.54E+02	9.70E+01	5.68E+01	5.68E+01		5.68E+01	2.86E+01	2.82E+01
Pu-240										
Pu-241										
Si-90	3.72E+03		3.72E+03	2.34E+03	1.37E+03	1.37E+03		1.37E+03	6.90E+02	6.81E+02
Y-90	3.72E+03		3.72E+03	2.34E+03	1.37E+03	1.37E+03		1.37E+03	6.90E+02	6.81E+02
Tc-99	6.16E+01		3.85E+01	2.27E+01	2.27E+01	2.27E+01		2.27E+01	1.14E+01	1.13E+01
Total Curies	1.42E+05		1.42E+05	8.92E+04	5.22E+04	5.22E+04		5.22E+04	2.63E+04	2.59E+04

Chemicals (kg)										
Ag+	2.83E+01		2.83E+01	1.78E+01	1.04E+01	1.04E+01		1.04E+01	5.25E+00	5.18E+00
Am+3	4.52E-03		4.52E-03	2.85E-03	1.67E-03	1.67E-03		1.67E-03	8.40E-04	8.28E-04
As+5										
B+3	5.14E+00		3.24E+00	1.90E+00	1.90E+00	1.90E+00		1.90E+00	9.55E-01	9.42E-01
Bar+2	4.93E+00		4.93E+00	3.11E+00	1.82E+00	1.82E+00		1.82E+00	9.17E-01	9.04E-01
Be+2										
Bi+3	1.56E+01		1.56E+01	9.87E+00	5.77E+00	5.77E+00		5.77E+00	2.91E+00	2.87E+00
Ca+2	5.78E+01		3.65E+01	2.13E+01	2.13E+01	2.13E+01		2.13E+01	1.07E+01	1.06E+01
Cd+2	1.26E+01		1.26E+01	7.96E+00	4.66E+00	4.66E+00		4.66E+00	2.34E+00	2.31E+00
Om+3	1.66E-07		1.66E-07	1.05E-07	6.12E-08	6.12E-08		6.12E-08	3.08E-08	3.04E-08
Co+3	4.04E-06		4.04E-06	2.55E-06	1.49E-06	1.49E-06		1.49E-06	7.51E-07	7.41E-07
Cs+	4.18E+00		2.64E+00	1.54E+00	1.54E+00	1.54E+00		1.54E+00	7.77E-01	7.66E-01
Cu+2	1.55E+00		1.55E+00	9.76E-01	5.71E-01	5.71E-01		5.71E-01	2.87E-01	2.84E-01
Eu+3										
Fe+3	1.16E+00		1.16E+00	7.30E-01	4.27E-01	4.27E-01		4.27E-01	2.15E-01	2.12E-01
Hg+2										
K+	3.35E+02		3.35E+02	2.12E+02	1.24E+02	1.24E+02		1.24E+02	6.23E+01	6.15E+01
La+3	1.64E-01		1.64E-01	1.04E-01	6.06E-02	6.06E-02		6.06E-02	3.01E-02	3.00E-02
Mg+2	1.13E+01		1.13E+01	7.14E+00	4.18E+00	4.18E+00		4.18E+00	2.10E+00	2.08E+00
Mn+4	5.11E+00		3.22E+00	1.89E+00	1.89E+00	1.89E+00		1.89E+00	9.49E-01	9.36E-01
Mo+6										
Ni+3	5.97E+04		5.97E+04	3.77E+04	2.20E+04	2.20E+04	3.65E+03	2.57E+04	1.29E+04	1.28E+04
Ni+2	3.33E+01		2.10E+01	1.23E+01	1.23E+01	1.23E+01		1.23E+01	6.18E+00	6.10E+00
Nm+4										
Pb+4	4.57E+01		2.88E+01	1.69E+01	1.69E+01	1.69E+01		1.69E+01	8.49E+00	8.39E+00
Pu+4	2.48E+00		2.48E+00	1.56E+00	9.15E-01	9.15E-01		9.15E-01	4.61E-01	4.55E-01
Se+6										
Si+4	1.78E+03		1.78E+03	1.12E+03	6.57E+02	6.57E+02		6.57E+02	3.31E+02	3.26E+02
Sm+4										
Sn+2	5.93E-01		5.93E-01	3.74E-01	2.19E-01	2.19E-01		2.19E-01	1.10E-01	1.09E-01
Ti+4										
UO2+2	1.74E+03		1.74E+03	1.10E+03	6.41E+02	6.41E+02		6.41E+02	3.23E+02	3.18E+02
W+6										
Zn+2										

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Chemicals (kg) (cont.)										
Zn+4	1.17E+02		1.17E+02	7.36E+01	4.31E+01	4.31E+01		4.31E+01	2.17E+01	2.14E+01
Al(OH)4-	9.50E+01		9.50E+01	6.00E+01	3.51E+01	3.51E+01		3.51E+01	1.77E+01	1.74E+01
Cl-	2.61E+03		2.61E+03	1.65E+03	9.63E+02	9.63E+02		9.63E+02	4.85E+02	4.78E+02
CO3-2										
Cr(OH)4-	1.47E+02		1.47E+02	9.27E+01	5.42E+01	5.42E+01		5.42E+01	2.73E+01	2.69E+01
F-	6.26E+02		6.26E+02	3.95E+02	2.31E+02	2.31E+02		2.31E+02	1.16E+02	1.15E+02
NO2-	3.28E+03		3.28E+03	2.07E+03	1.21E+03	1.21E+03	6.64E+02	1.89E+03	9.44E+02	9.32E+02
NO3-	1.65E+03		1.65E+03	1.04E+03	6.09E+02	6.09E+02		6.09E+02	3.07E+02	3.03E+02
OH-	7.11E+03		7.11E+03	4.49E+03	2.63E+03	2.63E+03	2.46E+03	5.08E+03	2.56E+03	2.52E+03
PO4-3	1.72E+03		1.72E+03	1.09E+03	6.35E+02	6.35E+02		6.35E+02	3.20E+02	3.15E+02
SO4-2	5.98E+03		5.98E+03	3.77E+03	2.21E+03	2.21E+03		2.21E+03	1.11E+03	1.10E+03
ToC4-	6.00E+00		6.00E+00	3.78E+00	2.21E+00	2.21E+00		2.21E+00	1.11E+00	1.10E+00
H2O	3.80E+06		3.80E+06	2.40E+06	1.40E+06	1.40E+06	1.44E+06	2.85E+06	1.43E+06	1.41E+06
Organic Carbon	6.12E+03		6.12E+03	3.86E+03	2.26E+03	2.26E+03		2.26E+03	1.14E+03	1.12E+03
ZrO2·2H2O	4.94E-01		4.94E-01	3.12E-01	1.82E-01	1.82E-01		1.82E-01	9.18E-02	9.06E-02
Hg										
Cl2										
CO2										
F2										
N2										
NO										
O2										
NH3										

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.25E+05		3.25E+05	1.09E+03	3.28E+05	3.28E+05		3.28E+05	1.08E+03	3.27E+05

Radionuclides (Ci)										
Am-241	2.27E+03		2.27E+03	7.49E+00	2.26E+03	2.26E+03		2.26E+03	7.47E+00	2.26E+03
C-14	3.56E-01		3.56E-01	1.18E-03	3.55E-01	3.55E-01		3.55E-01	1.17E-03	3.54E-01
Co-244										
Co-60	1.46E+02		1.46E+02	4.83E-01	1.46E+02	1.46E+02		1.46E+02	4.82E-01	1.46E+02
Cs-137	2.92E+05		2.92E+05	9.63E+02	2.91E+05	2.91E+05		2.91E+05	9.60E+02	2.90E+05
Ba-137	2.77E+05		2.77E+05	9.15E+02	2.76E+05	2.76E+05		2.76E+05	9.12E+02	2.75E+05
Eu-154										
Np-237										
Pu-239	3.42E+03		3.42E+03	1.13E+01	3.41E+03	3.41E+03		3.41E+03	1.13E+01	3.40E+03
Pu-240										
Pu-241										
Sr-90	2.81E+06		2.81E+06	9.25E+03	2.81E+06	2.81E+06		2.81E+06	9.26E+03	2.80E+06
Y-90	2.81E+06		2.81E+06	9.25E+03	2.81E+06	2.81E+06		2.81E+06	9.26E+03	2.80E+06
Tc-99	2.08E+02		2.08E+02	6.85E-01	2.07E+02	2.07E+02		2.07E+02	6.83E-01	2.06E+02
Total Curies	6.20E+06		6.20E+06	2.05E+04	6.18E+06	6.18E+06		6.18E+06	2.04E+04	6.16E+06

Chemicals (kg)										
Ag+	9.33E-02		9.33E-02	3.08E+00	9.30E-02	9.30E-02		9.30E-02	3.07E+00	9.27E-02
Al+3	4.52E+04		4.52E+04	1.49E+02	4.50E+04	4.50E+04		4.50E+04	1.48E+02	4.49E+04
Am+3	6.62E-01		6.62E-01	2.18E-03	6.60E-01	6.60E-01		6.60E-01	2.18E-03	6.59E-01
B+3	1.65E+01		1.65E+01	5.45E-02	1.65E+01	1.65E+01		1.65E+01	5.43E-02	1.64E+01
Be+2	5.26E+03		5.26E+03	1.74E+01	5.24E+03	5.24E+03		5.24E+03	1.73E+01	5.23E+03
Bi+3	5.27E+02		5.27E+02	1.74E+00	5.25E+02	5.25E+02		5.25E+02	1.73E+00	5.24E+02
Ca+2	1.33E+04		1.33E+04	4.39E+01	1.33E+04	1.33E+04		1.33E+04	4.39E+01	1.32E+04
Ca+2	4.03E+02		4.03E+02	1.33E+00	4.01E+02	4.01E+02		4.01E+02	1.32E+00	4.00E+02
Co+3	5.08E+00		5.08E+00	1.68E-02	5.06E+00	5.06E+00		5.06E+00	1.67E-02	5.05E+00
Cr+3	1.21E+03		1.21E+03	3.99E+00	1.21E+03	1.21E+03		1.21E+03	3.98E+00	1.20E+03
Cs+	1.78E+01		1.78E+01	5.87E-02	1.77E+01	1.77E+01		1.77E+01	5.86E-02	1.77E+01
Du+2	1.34E+02		1.34E+02	4.42E-01	1.34E+02	1.34E+02		1.34E+02	4.41E-01	1.33E+02
Fe+3	5.94E+04		5.94E+04	1.96E+02	5.92E+04	5.92E+04		5.92E+04	1.95E+02	5.90E+04
K+	1.50E+03		1.50E+03	4.93E+00	1.49E+03	1.49E+03		1.49E+03	4.92E+00	1.49E+03
La+3	2.07E+02		2.07E+02	6.84E-01	2.07E+02	2.07E+02		2.07E+02	6.82E-01	2.06E+02
Mg+2	6.91E+03		6.91E+03	2.28E+01	6.89E+03	6.89E+03		6.89E+03	2.27E+01	6.87E+03
Mn+4	2.43E+03		2.43E+03	8.01E+00	2.42E+03	2.42E+03		2.42E+03	7.99E+00	2.41E+03
Ng+	8.42E+04		8.42E+04	2.78E+02	8.40E+04	8.40E+04		8.40E+04	2.77E+02	8.37E+04
Ni+3	1.16E+03		1.16E+03	3.82E+00	1.15E+03	1.15E+03		1.15E+03	3.81E+00	1.15E+03
Pb+4	2.51E+03		2.51E+03	8.27E+00	2.50E+03	2.50E+03		2.50E+03	8.24E+00	2.49E+03
Pb+2	1.69E+02		1.69E+02	5.56E-01	1.68E+02	1.68E+02		1.68E+02	5.54E-01	1.67E+02
Pu+4	5.52E+01		5.52E+01	1.83E-01	5.50E+01	5.50E+01		5.50E+01	1.82E-01	5.49E+01
SI+4	7.64E+04		7.64E+04	2.52E+02	7.61E+04	7.61E+04		7.61E+04	2.51E+02	7.59E+04
SI+2	1.67E+02		1.67E+02	5.51E-01	1.66E+02	1.66E+02		1.66E+02	5.49E-01	1.66E+02
UO2+2	9.42E+02		9.42E+02	3.11E+00	9.39E+02	9.39E+02		9.39E+02	3.10E+00	9.36E+02
Zn+2	4.89E+01		4.89E+01	1.61E-01	4.87E+01	4.87E+01		4.87E+01	1.61E-01	4.86E+01
Zr+4	2.20E+03		2.20E+03	7.27E+00	2.20E+03	2.20E+03		2.20E+03	7.25E+00	2.19E+03
Cl-	5.64E+01		5.64E+01	1.86E-01	5.62E+01	5.62E+01		5.62E+01	1.86E-01	5.61E+01
F-	6.71E+01		6.71E+01	2.22E-01	6.69E+01	6.69E+01		6.69E+01	2.21E-01	6.67E+01
NO2-	1.25E+01		1.25E+01	4.13E-02	1.25E+01	1.25E+01		1.25E+01	4.12E-02	1.25E+01
NO3-	1.02E+01		1.02E+01	3.36E-02	1.02E+01	1.02E+01		1.02E+01	3.35E-02	1.01E+01
OH-	1.35E+04		1.35E+04	4.48E+01	1.35E+04	1.35E+04		1.35E+04	4.46E+01	1.35E+04
PO4-3	7.94E+03		7.94E+03	2.62E+01	7.91E+03	7.91E+03		7.91E+03	2.61E+01	7.89E+03
SO4-2	1.26E+02		1.26E+02	4.16E-01	1.26E+02	1.26E+02		1.26E+02	4.15E-01	1.25E+02
TOC6-	2.02E+01		2.02E+01	6.67E-02	2.02E+01	2.02E+01		2.02E+01	6.65E-02	2.01E+01

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Chemicals (kg) (cont.)										
Organic Carbon	2.04E+03		2.04E+03	6.73E+00	2.03E+03	2.03E+03		2.03E+03	6.71E+00	2.03E+03
ZnO:Zn2O	1.89E-03		1.89E-03	6.24E-06	1.89E-03	1.89E-03		1.89E-03	6.22E-06	1.89E-03
Ag2O										
Al2O3										
Am2O3										
As2O5										
B2O3										
BeO										
BeO										
Bi2O3										
CaO										
CdO										
Cr2O3										
Cr2O3										
Cs2O										
ClO										
Eu2O3										
Fe2O3										
K2O										
La2O3										
Li2O										
MgO										
MnO3										
Na2O										
Ni2O3										
NpO2										
P2O5										
PbO2										
PdO										
PluO2										
SeO3										
SiO2										
SO3										
SnO										
Ta2O7										
TiO2										
UO3										
VO3										
ZnO										
ZrO2										

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Total Mass Flow (kg)	1.45E+06	2.88E+06	1.45E+06	1.43E+06	3.73E+06	5.16E+06	6.80E+04		1.95E+05	
Volume (L)	1.44E+06	2.87E+06	1.45E+06	1.42E+06	3.73E+06	5.15E+06	2.89E+04		1.95E+05	
Specific Gravity	1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	2.41E+00		1.00E+00	

Radionuclides (Ci)										
Am-241		2.84E+00	1.43E+00	1.41E+00		1.41E+00	1.41E-02			
C-14							8.17E-04			
Am-244		2.46E-03	1.24E-03	1.22E-03		1.22E-03				
Co-60		8.39E-01	4.22E-01	4.15E-01		4.15E-01				
Cs-137		1.26E+04	6.34E+03	6.24E+03		6.24E+03	5.59E+06			
Ba-137		1.20E+04	6.02E+03	5.93E+03		5.93E+03	5.31E+06			
Eu-154							4.81E-02			
Np-237							3.59E-07			
Pl-239		2.82E+01	1.42E+01	1.40E+01		1.40E+01	3.15E-03			
Pl-240							7.87E-04			
Pl-241							6.04E-03			
Sm-90		6.81E+02	3.43E+02	3.39E+02		3.39E+02	2.07E+00			
Y-90		6.81E+02	3.43E+02	3.39E+02		3.39E+02	2.07E+00			
Tc-99		1.13E+01	5.69E+00	5.60E+00		5.60E+00	5.07E+02			
Total Curies		2.59E+04	1.31E+04	1.29E+04		1.29E+04	1.09E+07			

Chemicals (kg)										
Ag+		5.18E+00	2.61E+00	2.57E+00		2.57E+00	2.64E-06			
Am+3		8.28E-04	4.18E-04	4.11E-04		4.11E-04	4.12E-06			
As+5							2.33E-06			
B+3		9.42E-01	4.75E-01	4.67E-01		4.67E-01	2.46E-05			
Ba+2		9.04E-01	4.56E-01	4.49E-01		4.49E-01	3.50E-05			
Be+2							2.20E-13			
Bi+3		2.87E+00	1.45E+00	1.42E+00		1.42E+00	4.10E-06			
Ca+2		1.06E+01	5.34E+00	5.26E+00		5.26E+00	4.47E-02			
Ca+2		2.31E+00	1.17E+00	1.15E+00		1.15E+00	9.50E-06			
Cl-2		3.04E-08	1.53E-08	1.51E-08		1.51E-08				
Cl-3		7.41E-07	3.74E-07	3.68E-07		3.68E-07				
Cl-3		7.66E-01	3.86E-01	3.80E-01		3.80E-01	6.45E+01			
Cl-3		2.84E-01	1.43E-01	1.41E-01		1.41E-01	3.57E-06			
Eu+3							1.82E-07			
Fe+3		2.12E-01	1.07E-01	1.05E-01		1.05E-01	6.56E-02			
Hg+2							4.62E-06			
K+		6.15E+01	3.10E+01	3.05E+01		3.05E+01	3.22E-01			
La+3		3.01E-02	1.52E-02	1.49E-02		1.49E-02	3.50E-04			
Mg+2		2.08E+00	1.05E+00	1.03E+00		1.03E+00	1.01E-04			
Mn+4		9.36E-01	4.72E-01	4.64E-01		4.64E-01	2.19E-02			
Mo+6							2.83E-05			
Na+		1.64E+04	8.27E+03	8.14E+03		8.14E+03	3.26E+04			
Ni+3	3.65E+03	6.10E+00	3.07E+00	3.03E+00		3.02E+00	3.59E-02			
Np+4							5.10E-07			
Pb+4		8.39E+00	4.22E+00	4.16E+00		4.16E+00	1.44E-02			
Pl-24		4.55E-01	2.29E-01	2.25E-01		2.25E-01	5.43E-05			
Se+6							1.71E-07			
Si+4		3.26E+02	1.65E+02	1.62E+02		1.62E+02	1.75E-03			
Sn+4							1.36E-15			
Sm+2		1.09E-01	5.48E-02	5.39E-02		5.39E-02	1.47E-05			
Ti+4							1.68E-07			
UO2+2		3.18E+02	1.61E+02	1.58E+02		1.58E+02	1.43E-02			
W+6							5.97E-05			
Zn+2							2.00E-04			

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Chemicals (kg) (cont.)										
Zn+4		2.14E+01	1.08E+01	1.06E+01		1.06E+01	1.53E-06			
Al(OH) ₃ -		1.74E+01	8.78E+00	8.64E+00		8.64E+00	5.38E+00			
Cl-		4.78E+02	2.41E+02	2.37E+02		2.37E+02	3.15E-01			
CO ₃ -2							8.73E+00			
Cr(OH) ₃ -		2.69E+01	1.36E+01	1.34E+01		1.34E+01	5.87E-02			
F-		1.15E+02	5.78E+01	5.69E+01		5.69E+01	2.15E-01			
NO ₂ -	6.64E+02	1.60E+03	8.04E+02	7.91E+02		7.91E+02	1.07E+01			
NO ₃ -		3.03E+02	1.53E+02	1.50E+02		1.50E+02	3.16E+01			
OH-	2.46E+03	4.98E+03	2.51E+03	2.47E+03		2.47E+03	2.41E+04			
PO ₄ -3		3.15E+02	1.59E+02	1.56E+02		1.56E+02	5.31E-01			
SO ₄ -2		1.10E+03	5.53E+02	5.44E+02		5.44E+02	1.80E+00			
TcO ₄ -		1.10E+00	5.54E-01	5.45E-01	3.73E+06	5.45E-01	4.94E+01			
H ₂ O	1.44E+06	2.85E+06	1.44E+06	1.42E+06		5.15E+06	1.12E+04			
Organic Carbon		1.12E+03	5.65E+02	5.56E+02		5.56E+02	5.11E+00			
ZrO ₂ ·2H ₂ O		9.06E-02	4.57E-02	4.49E-02		4.49E-02				
Hg										
Cl ₂										
CO ₂										
F ₂										
N ₂										
NO										
O ₂										
NH ₃								1.95E+05		

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Total Mass Flow (kg)		3.27E+05	1.08E+05	3.26E+05		3.26E+05	1.80E+00	3.60E+05		9.19E+05
Radionuclides (Ci)										
Am-241		2.26E+03	7.44E+00	2.25E+03		2.25E+03	3.32E+02			2.58E+03
C-14		3.54E-01	1.17E-03	3.53E-01		3.53E-01				1.48E+02
Cm-244										1.22E-03
Co-60		1.46E+02	4.80E-01	1.45E+02		1.45E+02				1.48E+02
Cs-137		2.90E+05	9.57E+02	2.89E+05		2.89E+05				5.88E+05
Ba-137		2.75E+05	9.09E+02	2.75E+05		2.75E+05				5.59E+05
Eu-154										4.82E-02
Np-237										3.59E-07
Pu-239		3.40E+03	1.12E+01	3.39E+03		3.39E+03	1.50E+01			3.42E+03
Pu-240							3.75E+00			3.75E+00
Pu-241										6.04E-03
Sr-90		2.80E+06	9.23E+03	2.79E+06		2.79E+06	1.39E+05			2.93E+06
Y-90		2.80E+06	9.23E+03	2.79E+06		2.79E+06	1.39E+05			2.93E+06
Tc-99		2.06E+02	6.81E-01	2.06E+02		2.06E+02				7.19E+02
Total Curies		6.16E+06	2.03E+04	6.14E+06		6.14E+06	2.78E+05			1.73E+07
Chemicals (kg)										
Ag+		9.27E+02	3.06E+00	9.24E+02		9.24E+02				
Al+3		4.49E+04	1.48E+02	4.47E+04		4.47E+04				
Am+3		6.59E-01	2.17E-05	6.59E-01		6.59E-01	9.68E-02			
B+3		1.64E+01	5.41E-02	1.63E+01		1.63E+01				
Ba+2		5.23E+03	1.73E+01	5.21E+03		5.21E+03				
Bi+3		5.24E+02	1.73E+00	5.22E+02		5.22E+02				
Ca+2		1.32E+04	4.36E+01	1.32E+04		1.32E+04				
Ca+2		4.00E+02	1.32E+00	3.99E+02		3.99E+02				
Co+3		5.05E+00	1.67E-02	5.03E+00		5.03E+00				
Cr+3		1.20E+03	3.97E+00	1.20E+03		1.20E+03				
Cs+		1.77E+01	5.84E-02	1.76E+01		1.76E+01				
D+2		1.33E+02	4.39E-01	1.33E+02		1.33E+02				
Fe+3		5.90E+04	1.95E+02	5.88E+04		5.88E+04				
K+		1.49E+03	4.90E+00	1.48E+03		1.48E+03				
La+3		2.06E+02	6.80E-01	2.05E+02		2.05E+02				
Mg+2		6.87E+03	2.27E+01	6.84E+03		6.84E+03				
Mn+4		2.41E+03	7.90E+00	2.40E+03		2.40E+03				
Nb+		8.37E+04	2.76E+02	8.34E+04		8.34E+04				
Ni+3		1.15E+03	3.80E+00	1.15E+03		1.15E+03				
Pb+4		2.49E+03	8.21E+00	2.48E+03		2.48E+03				
Pd+2		1.67E+02	5.52E-01	1.67E+02		1.67E+02				
Pu+4		5.49E+01	1.81E-01	5.47E+01		5.47E+01	2.58E-01			
Si+4		7.59E+04	2.50E+02	7.56E+04		7.56E+04				
Sm+2		1.66E+02	5.47E-01	1.65E+02		1.65E+02	9.85E-01			
UO2+2		9.33E+02	3.09E+00	9.33E+02		9.33E+02				
Zn+2		4.86E+01	1.60E-01	4.84E+01		4.84E+01				
Zr+4		2.19E+03	7.22E+00	2.18E+03		2.18E+03				
Cl-		5.61E+01	1.85E-01	5.59E+01		5.59E+01				
F-		6.67E+01	2.20E-01	6.65E+01		6.65E+01				
NO2-		1.25E+01	4.11E-02	1.24E+01		1.24E+01				
NO3-		1.01E+01	3.34E-02	1.01E+01		1.01E+01				
OH-		1.35E+04	4.45E+01	1.34E+04		1.34E+04	4.64E-01			
PO4-3		7.89E+03	2.60E+01	7.86E+03		7.86E+03				
SO4-2		1.25E+02	4.14E-01	1.25E+02		1.25E+02				
TCO4-		2.01E+01	6.63E-02	2.00E+01		2.00E+01				
HNO2										3.81E+03

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Chemicals (kg) (cont.)										
Organic Carbon										
ZrO ₂ :2H ₂ O		2.03E+03	6.69E+00	2.02E+03		2.02E+03				
Ag ₂ O		1.89E-03	6.20E-06	1.87E-03		1.87E-03				
Al ₂ O ₃										9.95E+02
Am ₂ O ₃										8.45E+04
As ₂ O ₅										8.27E-01
B ₂ O ₃								4.59E+04		3.58E-06
BaO										4.60E+04
BeO										5.82E+03
Bi ₂ O ₃										6.12E-13
CaO										5.83E+02
Cd										1.84E+04
Ce ₂ O ₃										4.57E+02
Co ₂ O ₃										1.66E-08
Cr ₂ O ₃										7.08E+00
Cs ₂ O										1.76E+03
Cu ₂ O										8.74E+01
Eu ₂ O ₃										1.66E+02
Fe ₂ O ₃										2.11E-07
K ₂ O										8.40E+04
La ₂ O ₃										1.82E+03
Li ₂ O										2.41E+02
MgO								9.19E+03		9.19E+03
Mn ₂ O ₃										1.14E+04
Nb ₂ O ₅										4.24E-05
Ni ₂ O ₃										1.67E+05
Ni ₃ O ₂										1.62E+03
P ₂ O ₅										5.75E-07
PbO ₂										5.99E+03
Pd										2.87E+03
Plu ₂ O ₂										1.92E+02
Se ₂ O ₃										6.25E+01
SiO ₂								3.05E+05		2.75E-07
SO ₃										4.67E+05
SiO										5.59E+02
Ta ₂ O ₅										1.98E+02
TiO ₂										6.65E+01
U ₂ O ₃										2.80E-07
U ₃ O ₈										1.16E+03
VO ₃										7.53E-05
ZnO										6.03E+01
Zn ₃ O ₂										2.96E+03

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME		21
LIQUID COMPONENTS		
Total Mass Flow (kg)		5.19E+06
Volume (L)		5.19E+06
Specific Gravity		1.00E+00

Radionuclides (Ci)	
Am-241	
C-14	
Om-244	
Co-60	
Cs-137	
Ba-137	
Eu-154	
Np-237	
Plu-239	
Plu-240	
Plu-241	
Sr-90	
Y-90	
Tc-99	
Total Curies	

Chemicals (kg)	
Ag+	
Am+3	
As+5	
B+3	
Be+2	
Be+2	
Bi+3	
Ca+2	
Ca+2	
Cl+2	
Cl+3	
Co+3	
Co+3	
Cs+	
Cr+2	
Eu+3	
Fe+3	
Hg+2	
K+	
La+3	
Mg+2	
Mn+4	
Mn+6	
Nat	
Ni+3	
Np+4	
Pb+4	
Plu+4	
Se+6	
Si+4	
Sm+4	
Sr+2	
Ti+4	
UO2+2	
W+6	
Zn+2	

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	21
LIQUID COMPONENTS	

Chemicals (kg) (cont.)	
Zn+4	
Al(OH)+3	
Cl-	
CO3-2	
Cr(OH)+3	
F-	
NO2-	
NO3-	
OH-	
PO4-3	
SO4-2	
TeO4-	
H2O	5.18E+06
Organic Carbon	
ZrO2·2H2O	
Hg	4.62E-06
Cl2	2.93E+02
CO2	9.44E+03
F2	1.24E+02
N2	7.05E+01
NO	4.71E+02
O2	
NO3	1.42E+00

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Table 12 Phase 1 In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	21
SOLID COMPONENTS	
Total Mass Flow (kg)	
Radionuclides (Ci)	
Am-241	
C-14	
Cm-244	
Co-60	
Cs-137	
Ba-137	
Eu-154	
Np-237	
Pu-239	
Pu-240	
Pu-241	
Sr-90	
Y-90	
Tc-99	
Total Curies	
Chemicals (kg)	
Ag+	
Al+3	
Am+3	
B+3	
Ba+2	
Bi+3	
Ca+2	
Cd+2	
Co+3	
Cr+3	
Cs+	
Cu+2	
Fe+3	
K+	
La+3	
Mg+2	
Mn+4	
NH+	
Ni+3	
Pb+4	
Pd+2	
Pu+4	
Si+4	
Sr+2	
UO2+2	
Zn+2	
Zr+4	
Cl-	
F-	
NO2-	
NO3-	
OH-	
PO4-3	
SO4-2	
TeO4-	
MnO2	

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Table 12 Phase I In-Tank Sludge Washing of DST 241-AY-102/241-C-106 (36%/99% Retrieval) (12 sheets)

STREAM NAME	21
SOLID COMPONENTS	
Chemicals (kg) (cont.)	
Organic Carbon	
ZrO ₂ ·2H ₂ O	
Ag ₂ O	
Al ₂ O ₃	
Am ₂ O ₃	
As ₂ O ₅	
B ₂ O ₃	
BaO	
BeO	
Bi ₂ O ₃	
CaO	
Cd	
Cr ₂ O ₃	
Co ₂ O ₃	
Cr ₂ O ₃	
CS ₂ O	
D ₂ O	
Eu ₂ O ₃	
Fe ₂ O ₃	
K ₂ O	
La ₂ O ₃	
Li ₂ O	
MgO	
Mn ₂ O ₃	
Na ₂ O	
Ni ₂ O ₃	
NiO ₂	
P ₂ O ₅	
PbO ₂	
Pd	
Pu ₂ O ₂	
Se ₂ O ₃	
SiO ₂	
SO ₃	
SiO	
Ta ₂ O ₇	
TiO ₂	
U ₂ O ₃	
W ₂ O ₃	
ZnO	
ZrO ₂	

2.4 HIGH-LEVEL WASTE PRIVATE CONTRACTOR OPERATIONS

The Phase 1 HLW contractor returns entrained solids to the operating contractor, but incorporates the other intermediate waste products (strontium/TRU, CIP and TIP) into IHLW. The CIP (Stream 15 on Figure 8) contains "IX Material" that is assumed to become part of the dry, free-flowing product. Since the HLW contractor probably would not produce a dry, free-flowing CIP, "IX Material" is deleted from the CIP stream that is routed to HLW immobilization.

The major feed streams and products of HLW immobilization are depicted on Figures 10, 11, and 12. Sixteen batches of pretreated HLW solids are transferred to the HLW contractor: 2 from AZ-101, 2 from AZ-102 and 12 from AY-102. For this model, the HLW contractor divides the intermediate waste products equally between the 16 HLW feed batches.

The *PPTB* mass balances account for the vitrification of 375,000 kgs (oxide equivalent) of washed HLW. This exceeds the minimum order quantity (245,000 kgs), but falls short of the maximum order quantity (465,000 kgs). Future revisions of the *PPTB* will identify additional solids for Phase 1.

Glass formers (Stream 14 on Figure 10 and Stream 18 on Figures 11 and 12) are added to reach 25% waste oxide loading in the IHLW. No sodium, silicon or private contractor-added material counts toward the waste oxide loading. The mass balance also accounts for oxygen consumed in the cold cap and volatile species. With standard canisters containing a net 1650 kgs or 0.62 m³ per canister, PCI returns 910 standard canisters (350 from AZ-101/AZ-102 and 560 from AY-102/C-106). The number of canisters from each batch was previously summarized in Table S-1.

2.5 ENHANCED SLUDGE WASHING ADJUSTMENT

The *PPTB* does not model enhanced sludge washing (ESW) of Phase 1 HLW solids, but this section estimates the ESW effect on residual HLW solids. The *TWRS Process Flowsheet* used DST caustic leach factors of 85%, 75% and 70% for Al, Cr, and P, respectively. Since no new ESW data specific to NCAW is available, the same factors were used for AZ-101 and AZ-102. Experimental caustic leach factors for C-103 (same waste type as C-106) waste are available: 44%, 11%, and 43% for Al, Cr, and P, respectively. These were used for AY-102/C-106 waste.

AZ-101 and AZ-102 ESW waste oxides are approximately 75% of the water washed amount. AY-102/C-106 ESW waste oxides are approximately 82% of the water washed amount. The corresponding canister count is 725 (265 from AZ-101/AZ-102 and 460 from AY-102/C-106). This is equivalent to 300,000 kgs of washed HLW oxides, which exceeds the minimum order quantity of 245,000 kgs.

This estimate should be regarded cautiously in view of the tentative ESW data that it is based on.

3.0 PHASE 2 FLOWSHEET/MASS BALANCE

The operating contractor's Phase 2 function is limited to day-to-day management of tank waste (see Figure 1), while DOE will procure all retrieval and treatment services from private contractors. There are some programmatic planning assumptions available for Phase 2, but nothing equivalent to the Phase 1 RFP (DOE-RL 1996) to provide guidance on feed envelopes, separation requirements, product specifications, or how to distribute and schedule procured services among the Phase 2 private contractors.

In the absence of specific guidance, the PPTB models Phase 2 processing in a manner similar to the TWRs Process Flowsheet (Orme 1995). The feed stream to Phase 2 is a composite of the total tank inventory with appropriate adjustments to account for prior Phase 1 processing. The calculation engine underlying the Phase 2 flowsheet/mass balance is the TWRs Process Flowsheet ASPEN PLUS model that simulates waste processing in considerable detail.¹¹

The TWRs Process Flowsheet (Orme 1995) baseline architecture for sludge pretreatment is in-tank enhanced sludge washing. During FY-1995, a proposed change to out-of-tank enhanced sludge washing was postponed because of DOE's preference to maintain the same process baseline during the early stages of privatization negotiations. The change to an out-of-tank enhanced sludge washing architecture will be completed in FY-1997, and reflected in Revision 1 of the PPTB. A study addressing the tradeoffs of in-tank vs. out-of-tank pretreatment is available (Raytheon 1995).

A conceptual in-tank architecture is shown in Figure 13.

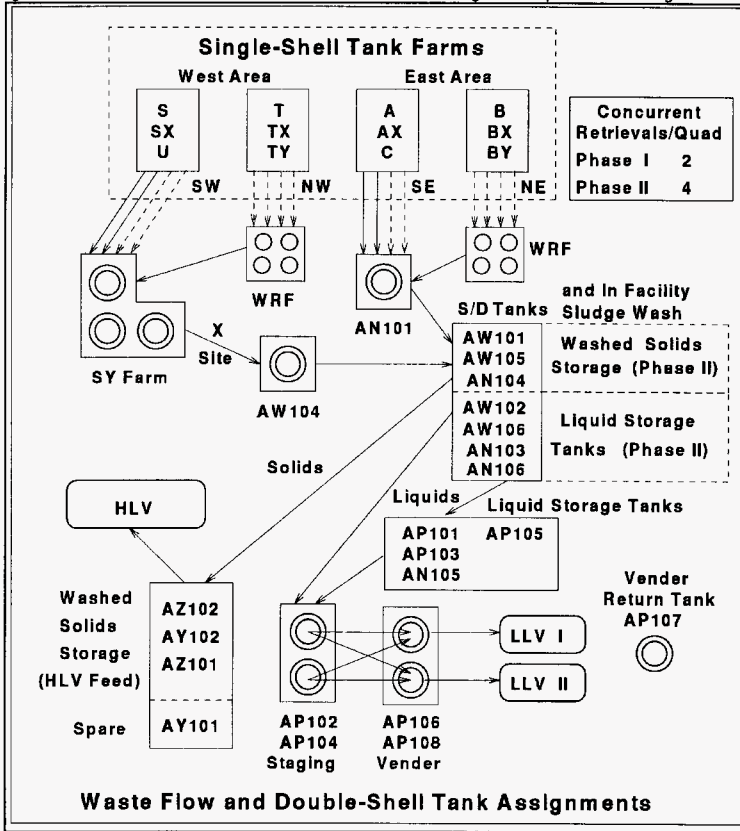
3.1 THE PHASE 2 FEED STREAM

3.1.1 Initial Wash

The retrieval of waste from different tanks constitutes an initial wash. The initial wash occurs during retrieval with dilute caustic, as salts are dissolved and insoluble solids are mobilized and dispersed through the slurry. The output from several simultaneous retrieval operations is accumulated in million-gallon staging tanks. Blending occurs when slurries from different sources are combined in the accumulation tanks. The energy and turbulence imparted to the slurries by sluicers, mixer pumps, transfer pumps, and the ensuing temperature rise are factors that affect the extent of the initial wash. This initial stage of washing and blending is actually allocated to the retrieval function. SY Tank Farm provides staging capacity for 200 West Area. Two 200 East Area DSTs are set aside for receiving retrieved waste.

¹¹Figure 14 (Phase 2 Waste Processing) and the associated mass balance in Table 13 reflect major streams, or combined streams extracted from the detailed model, to provide a summary level flowsheet of Phase 2.

Figure 13 Initial Wash and In-Tank Processing Conceptual Configuration¹²



¹²This tentative configuration has been used for sequence modelling studies (Penwell et al. 1996).

3.1.2 Total Composite Feed Stream

For flowsheet calculations, the retrieved waste is a 5M sodium slurry composited from the contents of all DSTs and SSTs. All of the water soluble components of the waste are in solution as a result of the initial retrieval wash. The total tank inventory (Stream 1 on Figure 14) is consistent with the total inventory from the TWRS Process Flowsheet (Orme 1995). The water soluble portion of the SST waste has been revised in accordance with the latest evaluation of water solubility, incorporating data from 18 additional SSTs (Colton 1996) than the 27 SSTs that were evaluated previously (Colton 1995). The liquid and solid distribution of DST waste was not revised because new data was not available.

3.1.3 Adjusted Composite Feed Stream

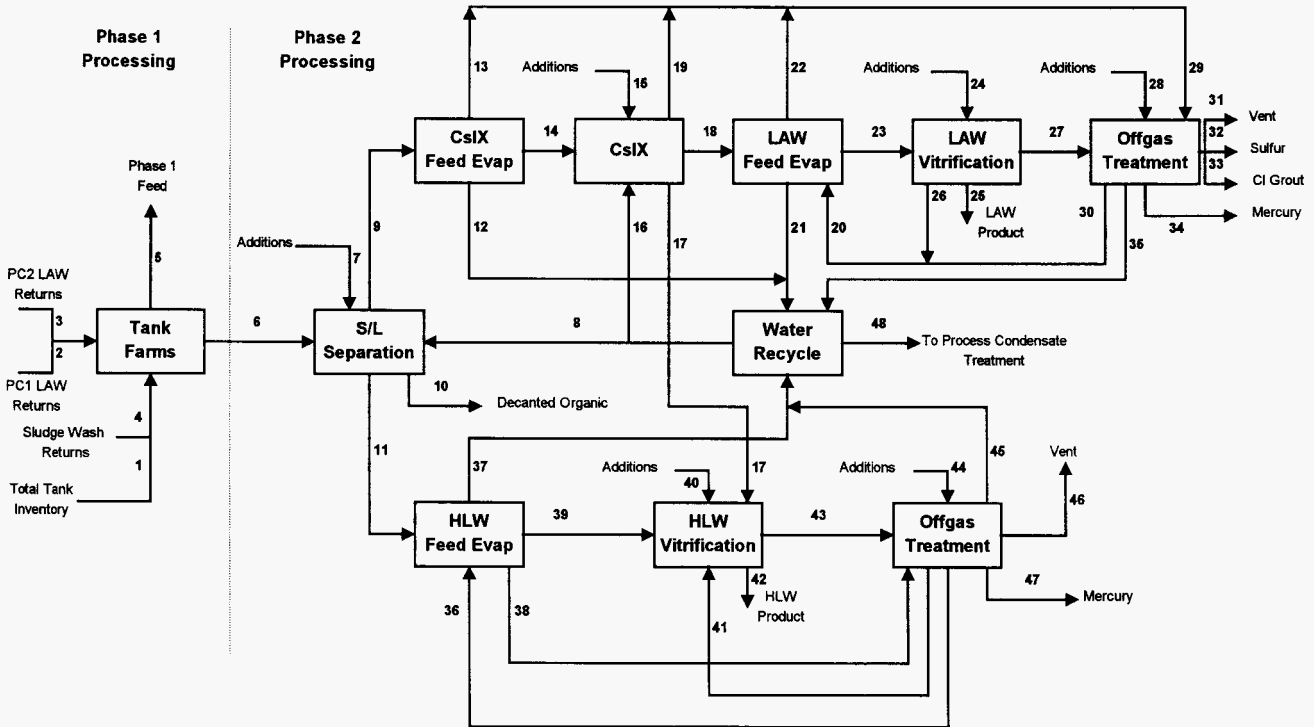
For Figure 14 and Table 13, the total tank inventory is adjusted to account for the Phase 1 sludge-washing operation, for the supernates and solids fed to the Phase 1 contractors (Stream 5), and for the intermediate products (Streams 2 and 3) returned by the Phase 1 private contractors. The resulting Stream 6 on Figure 14 is the composite feed to Phase 2. The TANK FARMS process block on Figure 14 performs the adjustment.

3.2 SOLID/LIQUID SEPARATIONS

The SOLID/LIQUID (S/L) SEPARATION process block includes the established TWRS Process Flowsheet steps of (1) initial separation of waste liquids from solids by settle/decant, (2) leaching of caustic soluble components, and (3) adjustment of the interstitial liquid concentration by repeated washings with dilute hydroxide/nitrite solution. To prevent adverse effects on downstream operations from organic phases that might be retrieved from some SSTs, the PPTB adds a new continuous decanter capability to separate organics from decanted supernates, leachates, and wash solutions. The amount of separable organic has been difficult to estimate and the assumed flowsheet value is 78,000 kg (Klem 1996).

The enhanced sludge-washing process utilizes leaching washes with 3 M caustic solution to remove selected components (primarily aluminum, chromium, phosphorus and sodium) from the tank waste sludges, followed by dilute caustic washes to remove the interstitial dissolved components. The process is based on experience at the Savannah River Site, and preliminary caustic washing results with a limited number of Hanford sludge samples (Colton 1996). Initial indications from process mass balance calculations are that the HLW oxides remaining after enhanced sludge washing will be approximately 75% of the amount remaining after simple water washing alone.

Figure 14 Phase 2 Waste Processing



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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Total Mass Flow (MT)	7.21E+05	3.73E+03	3.77E+03	9.46E+03	9.57E+04	6.42E+05	3.38E+04	4.88E+05	1.00E+06	7.79E+01
Volume (L)	5.89E+08	3.69E+06	3.71E+06	9.28E+06	7.34E+07	5.32E+08	2.26E+07	4.88E+08	8.72E+08	7.79E+04
Specific Gravity	1.23E+00	1.01E+00	1.02E+00	1.02E+00	1.30E+00	1.21E+00	1.50E+00	1.00E+00	1.15E+00	1.00E+00

Radionuclides (Ci)										
Am-241	8.00E+03	6.11E+00	5.90E+00	1.15E+02	3.35E+03	4.77E+03		4.61E-04	4.76E+03	
C-14	3.22E+03	2.09E-01	1.89E-01	3.72E+01	3.78E+02	2.88E+03		2.78E-04	2.87E+03	
Ca-137	3.10E+07	5.96E+04	3.99E+04	1.65E+06	2.70E+07	6.07E+06		4.47E-01	1.39E+07	
Ba-137	3.02E+07	5.67E+04	3.79E+04	1.10E+06	2.57E+07	5.77E+06		4.23E-01	1.32E+07	
Np-237	6.94E+00	1.60E-03	7.43E-04		3.84E-01	6.58E+00		1.34E-04	6.57E+00	
Ru-239	1.65E+03	1.16E+00	1.03E+00		6.32E+02	1.16E+03		1.12E-04	1.16E+03	
Ru-240	3.40E+02	2.90E-01	2.61E-01	1.45E+02	1.10E+02	3.20E+02		3.09E-05	3.19E+02	
Ru-241	4.76E+03	1.81E+00	1.62E+00		6.90E+02	4.08E+03		3.94E-04	4.07E+03	
Sr-90	1.88E+06	2.02E+03	2.39E+03	3.84E+04	1.21E+06	7.12E+05		6.88E-02	7.10E+05	
Y-90	1.88E+06	2.02E+03	2.39E+03	3.84E+04	1.21E+06	7.12E+05		6.88E-02	7.10E+05	
Tc-99	2.27E+04	1.73E+01	5.78E+02	1.71E+02	7.04E+03	1.64E+04		3.54E-03	1.64E+04	
Total Carries	6.58E+07	1.20E+05	8.31E+04	2.34E+06	5.51E+07	1.33E+07		1.01E+00	2.83E+07	

Chemicals (MT)										
Ag+	3.20E-01	2.22E-06	1.85E-06	2.57E-02	2.91E-02	3.16E-01		3.06E-08	3.16E-01	
Am3	2.53E+03	1.78E-06	1.74E-06	3.36E-05	9.74E-04	1.39E-03		1.34E-10	1.39E-03	
As3	4.03E-05				4.05E-05					
BH3	3.43E-02	3.01E-05	3.98E-05	5.05E-03	2.20E-02	1.74E-02		1.68E-09	1.73E-02	
Be+2	7.91E-01	1.01E-05	2.19E-05	4.54E-03	1.19E-02	7.84E-01		7.57E-08	7.82E-01	
Be+2	2.43E-05				2.43E-05					
BH3	3.01E+00	2.21E-06	1.46E-06	1.43E-02	1.64E-02	3.01E+00		3.66E-07	3.77E+00	
Ca+2	1.52E+01	9.85E-03	1.04E-02	5.41E-02	4.30E+00	1.10E+01		1.12E-04	1.36E+01	
CaH2	7.63E+00	1.43E-04	1.48E-04	1.15E-02	7.21E-02	7.57E+00		1.01E-06	7.53E+00	
CaH3	2.65E+00			7.78E-04	6.17E-03	2.36E+00		2.28E-07	2.33E+00	
CaH3	9.50E-08				2.28E-07					
Ca+3	1.46E-03			9.59E-08	7.47E-07	1.46E-03		1.41E-10	1.46E-03	
Ca+	2.14E+00	6.89E-04	4.61E-04	5.29E-02	6.10E-01	1.58E+00		5.77E-08	1.84E+00	
Ca+2	9.83E-02	1.03E-04	1.05E-04	1.47E-03	4.48E-02	5.57E-02		5.39E-09	5.56E-02	
Fe+3	1.32E+01	1.32E-02	1.33E-02	1.46E-03	5.51E+00	7.72E+00		8.77E-07	9.04E+00	
H+										
Hg+2	5.84E-02	1.42E-04	1.42E-04		5.72E-02	1.49E-03		1.44E-10	1.49E-03	
K+	7.07E+02	8.17E-01	8.00E-01	4.17E-01	3.21E+02	3.88E+02		3.78E-05	3.87E+02	
La+3	2.39E-01	8.95E-05	2.15E-04	2.51E-04	6.40E-02	1.75E-01		1.70E-08	1.75E-01	
Mg+2	1.46E-04				1.46E-04					
Mn+2	4.83E-05				4.83E-05					
Mn+4	1.03E+01	5.03E-03	5.10E-03	4.68E-03	2.10E+00	8.73E+00		4.68E-12	4.84E-05	
Mn+6	2.23E-03				7.23E-03			8.43E-07	8.71E+00	
Na+	6.57E+04	2.50E+01	3.48E+01	1.31E+02	1.06E+04	5.52E+04	9.20E+03	8.28E-13	4.43E-13	
Ni+3	8.21E+00	7.07E-03	7.24E-03	3.03E-02	3.03E+00	5.22E+00		5.04E-07	5.21E+00	
Ni+4	9.83E-03	2.27E-06	1.03E-06		5.45E-04	9.33E-03		1.89E-07	9.33E-03	
Fe+4	9.59E+00	6.32E-03	6.32E-03	4.18E-02	2.61E+00	7.05E+00		9.51E-07	7.04E+00	
Pu+4	2.86E-02	2.00E-05	1.78E-05	2.33E-03	1.07E-02	2.02E-02		1.95E-09	2.02E-02	
RF+	2.40E-04				2.40E-04			2.32E-11	2.40E-04	
Ru+7	1.08E-04				4.21E-04					
Ru+3	8.50E-04				4.19E-03					
Ru+3	1.18E-03				1.39E-03					
Sr+6	4.35E-04				5.93E-04					
Si+4	7.06E+01	8.64E-03	5.08E-03	1.84E+00	5.94E+00	6.65E+01		1.32E-09	8.72E-10	
Sn+2	3.81E-01	1.43E-05	1.69E-05	1.74E-03	1.74E-02	3.65E-01		3.52E-08	3.64E-01	
Ta+6	8.27E-04				4.80E-03					
UO2+2	4.13E+01				1.26E+01	3.10E+01		6.11E-06	6.25E+01	
Zn+2	2.78E-04				7.78E-04					
Al(CH3)4-	8.06E+03	8.99E+00	8.90E+00	1.64E+01	3.72E+03	4.38E+03		9.07E-04	9.29E+03	
Cl-	6.78E+02	4.99E-01	5.05E-01	2.45E+00	2.03E+02	4.79E+02		2.70E-05	1.78E-05	
CO3-2	3.10E+03	3.87E+00	3.63E+00	2.35E+01	1.69E+03	1.44E+03		3.71E-04	4.78E+02	
Cr(CH3)4-	4.83E+02	1.03E-01	7.60E-02	1.12E+00	4.14E+01	4.43E+02		5.84E-05	4.46E+03	
F-	1.14E+03	2.46E-01	2.38E-01	1.67E+00	1.05E+02	1.04E+03		2.29E-04	1.04E+03	
I2-	9.07E-02				5.05E-05	8.99E-02		6.41E-07	8.97E-02	
NiO-	9.50E+03	9.33E+00	8.99E+00	4.04E+01	3.93E+03	5.59E+03	2.34E+02	5.67E-05	5.74E+03	
NO3-	1.07E+05	1.88E+01	1.90E+01	3.85E+01	7.94E+03	9.94E+04		2.35E-02	9.92E+04	
OH-	8.53E+03	4.21E+00	1.15E+01	1.99E+01	1.72E+03	6.82E+03	6.72E+03	1.09E-03	1.33E+04	
RO4-3	4.56E+03	3.17E-01	3.22E-01	1.38E+00	1.32E+02	4.43E+03		6.41E-07	6.97E-02	
SD4-2	2.02E+03	1.04E+00	8.41E-01	1.23E+01	4.20E+02	1.62E+03		1.57E-04	1.61E+03	
TeO4-	2.21E+00	1.70E-03	5.63E-02	1.67E-02	6.85E-01	1.60E+00		3.44E-07	1.60E+00	
H2O	5.08E+05	3.67E+03	3.68E+03	9.16E+03	6.41E+04	4.61E+05	1.75E+04	4.88E+05	7.98E+05	
Separable Organic	1.80E+01				7.80E+01					
Organic Carbon	1.06E+03	1.67E+00	1.78E+00	6.59E+00	7.34E+02	3.37E+02		1.02E-04	3.36E+02	7.79E+01
ZnO2.2H2O	7.53E+00			6.08E-04	1.74E-03	7.53E+00		7.27E-07	7.51E+00	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Chemicals Continued (MT)										
He								8.69E-09	5.73E-09	
TeO2								4.53E-12	2.99E-12	
Cl2										
CO										
CO2										
F2										
H2										
I2										
N2										
N2O										
NO										
NE2										
O2										
SO2										
Glycolic Anion								1.75E-07	1.16E-07	
H2S										
Glycolic Acid										
Kerosene										
NE3										
Polyelectrolyte										
Sulfur							1.54E+02	1.92E+06	1.71E+01	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (MT)	2.23E+04		4.35E-03	5.04E+00	5.53E+02	2.17E+04			1.96E+02	
Radionuclides (Ci)										
Am-241	9.75E+04		7.38E+02	2.88E+02	3.76E+04	6.11E+04			8.03E+02	
C-14	2.12E+03			1.64E-01	2.11E+01	2.10E+03			2.75E+01	
Cs-137	1.39E+07			6.01E+03	6.81E+05	1.32E+07			7.01E+04	
Ba-137	1.32E+07			5.71E+03	6.47E+05	1.26E+07			6.66E+04	
Po-237	6.27E+01					6.27E+01			6.25E-01	
Ru-239	2.55E+04					2.12E+04			2.78E+02	
Ru-240	6.26E+03		3.35E+01	3.99E+01	4.19E+03	6.28E+03			8.25E+01	
Ru-241	6.99E+04					6.99E+04			9.14E+02	
Sr-90	5.18E+07					4.28E+07			5.62E+05	
Y-90	5.18E+07		3.42E+05	7.72E+04	9.99E+06	4.28E+07			5.62E+05	
Tc-99	9.32E+03			3.79E+00	4.29E+02	8.87E+03			1.17E+02	
Total Curies	1.31E+08		6.85E+05	1.67E+05	2.02E+07	1.12E+08			1.26E+06	
Chemicals (MT)										
Ag+	1.49E+00			9.25E-03	9.33E-01	5.56E-01			7.31E-03	
Al+3	2.43E+03			6.07E-01	6.50E+01	2.37E+03			1.23E+01	
Am+3	2.84E-02		2.15E-04	8.38E-05	1.10E-02	1.78E-02			2.34E-04	
As+5	2.26E-03				2.26E-03					
Ba+2	3.74E+00				3.74E+00					
Be+2	3.08E-03				3.08E-03					
Bi+3	2.60E+02			5.20E-03	5.27E-01	2.59E+02			3.40E+00	
Ca+2	1.46E+02			1.40E-01	1.43E+01	1.32E+02			1.70E+00	
CaH2	6.59E+00			3.76E-02	4.23E+00	2.37E+00			3.11E-02	
Ca+3	2.35E+02			3.04E-03	3.95E-01	2.35E+02			3.09E+00	
Cl+3	1.76E-05			9.16E-08	1.20E-05	5.71E-06			7.51E-08	
Co+3	4.08E-02			5.02E-05	5.08E-03	3.58E-02			4.70E-04	
Cr+3	1.43E+02			1.52E-02	1.60E+00	1.42E+02			1.63E+00	
Cr+	4.73E-01			3.16E-04	3.53E-02	4.38E-01			2.32E-03	
Cl+2	1.86E-01				1.86E-01					
Fe+3	7.84E+02			9.50E-01	1.04E+02	6.81E+02			8.93E+00	
Hg+2	8.81E-02				8.81E-02				1.16E-03	
K+	2.96E+01			2.11E-02	2.37E+00	2.72E+01			3.58E-01	
La+3	2.30E+01			1.51E-02	1.80E+00	2.13E+01			2.79E-01	
Mg+2	6.22E+00			7.07E-02	7.21E+00	1.12E+00			1.47E-02	
Mn+6	1.80E+02			3.32E-02	3.59E+00	1.76E+02			2.32E+00	
Mb+6	3.21E-02			1.18E-04	1.58E-02	1.63E-02			2.15E-04	
Na+	3.10E+03			9.25E-01	9.50E+01	3.01E+03			2.18E+01	
Ni+3	2.06E+02			3.28E-02	3.63E+00	2.02E+02			2.66E+00	
Np+4	8.90E-02					8.90E-02			1.17E-03	
Pb+4	2.93E+01			2.73E-02	2.82E+00	2.63E+01			3.49E-01	
Ru+4	4.36E+01			6.43E-04	6.77E-02	3.70E-01			4.86E-03	
Ru+3	1.93E-01			1.32E-03	1.63E-01	2.96E-02			3.90E-04	
Se+6	3.31E+00			4.27E-03	5.61E-01	2.76E+00			3.62E-02	
Si+4	6.22E+02			1.75E-01	7.84E+01	5.44E+02			6.29E+00	
Sn+2	3.56E+01		2.43E-03	3.40E-03	3.99E-01	3.62E+01			4.75E-01	
Ti+4	2.78E+00			1.75E-03	2.66E-01	2.52E+00			3.32E-02	
Ti+4	1.55E-01				1.55E-01					
UD+2	1.61E+03			4.15E-02	4.65E+00	1.61E+03			2.07E+01	
Zn+2	5.06E-01			1.30E-03	1.61E-01	3.47E-01			4.52E-03	
Cl-	8.99E+00			9.68E-04	1.06E-01	8.90E+00			1.17E-01	
CO3-2	1.09E+02			1.55E-01	1.68E+01	9.25E+01			1.22E+00	
F-	6.82E+01			1.75E-03	2.21E-01	6.80E+01			8.94E-01	
I-	1.40E+03			2.89E-06	3.66E-04	1.04E+03			1.36E-05	
NO2-	6.18E+01			1.66E-02	2.19E+00	5.96E+01			7.84E-01	
NO3-	9.85E+02			1.01E-02	1.43E+00	9.85E+02			1.30E+01	
OH-	9.42E+03		1.13E-03	8.81E-01	1.05E+02	9.25E+03			7.31E+01	
RO4-3	4.95E+02			7.91E-02	8.04E+00	4.67E+02			1.94E+00	
SO4-2	4.18E+01			1.51E-03	1.94E-01	4.16E+01			5.47E-01	
TeO4-	9.07E-01			3.69E-04	4.17E-02	8.64E-01			1.14E-02	
H2O										
H2O2										
Organic Carbon	8.73E+01			3.67E-02	4.32E+00	8.30E+01			1.09E+00	
ZnO2.ZH2O	1.20E+03			1.42E-01	1.88E+01	1.18E+03			1.56E+01	
Ag2O										
Al(OH)3										
Al2O3										
Am2O3										
B2O3										
BaO										
Bi2O3										
CaO										

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Chemicals Continued (MT)										
CdO										
Ca2O3										
Ca2O8										
Ca2O3										
Ca2O										
ClO										
Fe2O3										
He										
HgO										
K2O										
La2O3										
Li2O										
MgO										
MnO										
MnO3										
Na2O										
Ni2O3										
BiO2										
PbO2										
Pb2O										
Pb2O3										
SeO3										
SiO2										
SO3										
SnO										
Ta2O7										
TiO2										
UO3										
ZnO										
ZrO2										
Cement										
Flyash										
Polyelectrolyte										
CS-100 - Na Foam									1.32E+00	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Total Mass Flow (MT)	1.70E+05	4.63E+05	5.14E+03	5.33E+05	7.82E+04	1.20E+04	9.54E+03	6.13E+05	1.01E+03	8.14E+05
Volume (L)	1.27E+05	4.21E+04	1.22E-03	4.02E+08	7.63E+07	1.20E+07	8.57E+06	5.84E+05	1.00E+06	6.01E+08
Specific Gravity	1.01E+00	1.00E+00	1.00E+00	1.32E+00	1.02E+00	1.00E+00	1.11E+00	1.27E+00	1.01E+00	1.02E+00
Radionuclides (Cl)										
Am-241	9.37E+00	4.17E-04	4.17E-07	4.76E+03				1.13E-05		4.76E+03
C-14	5.63E+00	2.52E-04	2.52E-07	2.87E+03				6.81E-06		2.87E+03
Cs-137							1.33E+07			
Ba-137	1.20E+05	1.15E+00	1.15E-03	1.32E+07			1.04E-02			
Np-237	1.30E-02	5.73E-07	5.73E-10	6.57E+00			3.27E-06			6.57E+00
Ru-239	2.28E+00	1.02E-04	1.02E-07	1.16E+03			2.73E-06			1.16E+03
Ru-240	6.28E-01	2.79E-05	2.79E-08	3.18E+02			7.57E-07			3.18E+02
Ru-241	8.01E+00	3.56E-04	3.57E-07	4.07E+03			6.65E-06			4.07E+03
Sr-90	1.40E+03	6.22E-02	6.22E-05	7.10E+05			1.69E-03			7.10E+05
Y-90	1.40E+03	6.22E-02	6.22E-05	7.10E+05			1.69E-03			7.10E+05
Tc-99	1.23E+01	1.44E-03	1.44E-06	1.64E+04			8.67E-05			1.64E+04
Total Curies	2.50E+05	2.49E+00	2.50E-03	2.85E+07			2.49E-02	2.59E+07	2.59E+06	1.99E-02
										6.83E+05
Chemicals (MT)										
Ag+	6.21E-04	2.76E-08	2.77E-11	3.16E-01				7.49E-10		3.16E-01
Am3	2.73E-06	1.22E-10	1.22E-13	1.39E-03				5.29E-12		1.39E-03
As+5										
BH3	3.41E-05	1.52E-09	1.52E-12	1.73E-02				4.11E-11		1.73E-02
Bat2	1.54E-03	6.85E-08	6.86E-11	7.82E-01				1.86E-09		7.82E-01
Be#2										
Bi+3	1.72E-02	3.30E-07	3.30E-10	3.77E+00				8.96E-09		3.77E+00
Ca#2	5.99E-02	1.19E-06	1.19E-09	1.36E+01				2.73E-06		1.36E+01
CH2	1.49E-02	6.62E-07	6.62E-10	7.53E+00				2.47E-08		7.53E+00
Co#3	4.63E-03	2.06E-07	2.06E-10	2.35E+00				5.59E-09		2.35E+00
Cm#3										
Co#3	2.87E-06	1.28E-10	1.28E-13	1.46E-03				3.46E-12		1.46E-03
Cr+	6.91E-03	1.61E-07	1.61E-10	1.84E+00				1.42E-09		1.84E+00
Cu#2	1.10E-04	4.87E-09	4.87E-12	5.65E-02			1.76E+00			5.65E-02
Fe#3	3.48E-02	7.92E-07	7.92E-10	9.04E+00				2.15E-08		9.04E+00
H+					1.88E+01					
H#2	2.92E-06	1.30E-10	1.30E-13	1.48E-03				3.50E-12		1.48E-03
K+	7.62E-01	3.39E-05	3.39E-08	3.87E+02				9.25E-07	1.58E+00	3.87E+02
La#3	3.45E-04	1.53E-08	1.53E-11	1.75E-01				4.15E-10		1.75E-01
M#2										
M#2	9.52E-08	4.24E-12	4.24E-15	4.84E-05				1.15E-13		4.84E-05
M#4	1.71E-02	7.63E-07	7.64E-10	8.71E+00				2.07E-08		8.71E+00
M#6	2.82E-13	4.78E-23	5.45E-13					2.02E-14		5.45E-13
Na+	6.67E+02	2.51E-02	2.51E-05	6.51E+04			8.39E+02	4.43E+02		5.17E+04
Ni#3	1.03E-02	4.58E-07	4.57E-10	5.21E+00				1.24E-08		5.21E+00
N#4	1.84E-05	8.16E-10	8.16E-13	9.31E-03				4.64E-09		9.31E-03
Ob#4	1.39E-02	6.16E-07	6.17E-10	7.04E+00				2.33E-08		7.04E+00
Or#4	3.97E-05	1.77E-09	1.77E-12	2.02E-02				4.78E-11		2.02E-02
Or+	4.72E-07	2.10E-11	2.10E-14	2.40E-04				5.69E-13		2.40E-04
Re#7										
Rn#3										
Rn#3										
Ser#3										
Se#5	4.51E-10	7.64E-17	7.64E-20	8.72E-10				3.24E-11		8.72E-10
Si#4	1.15E+00	1.19E-05	1.19E-08	1.36E+02				3.25E-07		1.36E+02
Sn#2	7.16E-04	3.19E-08	3.19E-11	3.64E-01				8.63E-10		3.64E-01
Ter#										
UD#2	5.25E-01	5.48E-06	5.48E-09	6.25E+01				1.50E-07		6.25E+01
Zn#2										
Al(OH)4-	8.09E+01	8.13E-04	8.14E-07	9.29E+03				2.22E-05		9.29E+03
BCL	9.21E-04	1.56E-12	1.56E-15	1.78E-05				6.62E-07		1.78E-05
Cl-	9.41E-01	1.26E-04	1.26E-07	4.78E+02				9.09E-06		4.78E+02
CO3-2	2.84E+00	1.26E-04	1.26E-07	1.44E+03				9.41E-07		1.09E+03
Cr(OH)4-	1.34E+00	4.16E-05	4.16E-08	4.75E+02				1.13E-06		4.75E+02
F-	1.08E+03	9.06E-05	9.07E-08	1.04E+03				5.62E-06		1.04E+03
I-	1.77E-04	7.83E-09	7.86E-12	8.97E-02				1.57E-08		8.97E-02
NO2-	8.81E+01	5.02E-04	5.03E-07	5.74E+03	5.00E-04			1.39E-05	5.00E-04	5.74E+03
NO3-	1.93E+02	2.61E-02	2.61E-05	9.92E+04	1.16E+03			5.73E-04	1.16E+03	9.92E+04
OH-	3.83E+02	1.18E-03	1.18E-06	1.33E+04	6.21E+02			2.67E-05	1.46E+01	1.33E+04
FO4-3	1.36E+01	4.17E-04	4.17E-07	4.76E+03				1.34E-05		4.76E+03
SO4-2	3.17E+00	1.41E-04	1.41E-07	1.61E+03				3.84E-06		1.61E+03
TCO4-	3.14E-03	1.40E-07	1.40E-10	1.60E+00				8.44E-09		1.60E+00
H2O	1.08E+05	4.63E+05	5.14E+03	5.33E+05	7.55E+04			1.20E+04	7.93E+03	1.08E+05
Separable Organic	1.53E-01							4.73E-10		4.73E-10
Organic Carbon	6.62E-01	1.14E-04	1.14E-07	3.36E+02				2.50E-06		3.36E+02
ZrO2 .2H2O	1.46E-02	6.59E-07	6.59E-10	7.51E+00				1.78E-08		7.51E+00

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Chemicals Continued (MT)										
H ₂										
TCO2	2.96E-09	5.02E-16	5.02E-19	5.73E-09		2.13E-10		5.94E-09		2.90E-07
Cl2	1.54E-12		2.62E-22	2.99E-12		1.11E-13		3.10E-12		6.46E-05
CO2									2.54E+02	
F2										
HE										
LD										
NE										
NO										
NO2										
O2										
SO2										
Glycolic Anion	5.96E-08	1.01E-14	1.01E-17	1.16E-07		4.30E-09		1.20E-07		
H2S										
Glycolic Acid										
Kerosene										
NE										
Polyelectrolyte	2.09E+00	1.50E-06	1.50E-09	1.71E+01		4.70E-08		1.71E+01		
Sulfur										

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Total Mass Flow (MT)	1.48E+04			1.96E+02	6.68E+02			8.64E+02		1.91E+04
Radionuclides (Ci)										
Am-241	6.03E+04			8.03E+02				8.03E+02		2.35E+02
C-14	2.07E+03			2.75E+01				2.75E+01		
Ce-137	5.25E+06			7.01E+04				7.01E+04		2.76E+04
Ba-137	4.99E+06			6.66E+04				6.66E+04		2.62E+04
Np-237	6.19E+01			8.23E-01				8.23E-01		3.48E-02
Ru-239	2.09E+04			2.78E+02				2.78E+02		6.07E+01
Ru-240	6.19E+03			8.25E+01				8.25E+01		1.69E+01
Ru-241	6.86E+04			9.14E+02				9.14E+02		2.10E+02
Sr-90	4.22E+07			5.62E+05				5.62E+05		5.37E+04
Y-90	4.22E+07			5.62E+05				5.62E+05		5.37E+04
Tc-99	8.76E+03			1.17E+02				1.17E+02		6.96E+02
Total Curies	9.48E+07			1.26E+06				1.26E+06		1.62E+05
Chemicals (MT)										
As+	5.49E-01			7.31E-03				7.31E-03		
Al+3	9.39E+02			1.25E+01				1.25E+01		
Am+3	1.76E-02			2.34E-04				2.34E-04		
As+5										
Ba+2										
Ba+3	2.55E+02			3.40E+00				3.40E+00		
Ca+2	1.28E+02			1.70E+00				1.70E+00		3.17E+02
Cl-2	2.36E+00			3.11E-02				3.11E-02		
Ca+3	2.32E+02			3.09E+00				3.09E+00		
Cl+3	5.64E-06			7.51E-08				7.51E-08		
Co+3	3.53E-02			4.70E-04				4.70E-04		
Cr+3	1.26E+02			1.63E+00				1.63E+00		
Cr+6	1.74E-01			2.32E-03				2.32E-03		
Cr+2										
Fe+3	6.71E+02			8.93E+00				8.93E+00		
Hg+2	8.70E-02			1.16E-03				1.16E-03		
K+	2.69E+01			3.58E-01				3.58E-01		
La+3	2.10E+01			2.79E-01				2.79E-01		
Mg+2	1.10E+00			1.47E-02				1.47E-02		
Mn+4	1.74E+02			2.32E+00				2.32E+00		
Mn+6	1.61E-02			2.15E-04				2.15E-04		
Na+	1.64E+03			2.18E+01				2.18E+01		
Ni+3	2.00E+02			2.66E+00				2.66E+00		
Ni+4	8.78E-02			1.17E-03				1.17E-03		4.93E-05
Pb+4	2.62E+01			3.49E-01				3.49E-01		
Pu+4	3.65E-01			4.86E-03				4.86E-03		
Rn+3	2.93E-02			3.90E-04				3.90E-04		
Sr+6	2.72E+00			3.62E-02				3.62E-02		
Si+4	4.68E+02			6.23E+00				6.23E+00		
Se+2	3.57E+01			4.75E-01				4.75E-01		
Th+4	2.49E+00			3.32E-02				3.32E-02		
Ti+4										
UO2+2	1.55E+03			2.07E+01				2.07E+01		
Zn+2	3.42E-01			4.53E-03				4.53E-03		
Cl-	4.78E+00			1.17E-01				1.17E-01		4.77E+00
CO3-2	9.12E+01			1.22E+00				1.22E+00		
F-	6.71E+01			8.94E-01				8.94E-01		1.91E+02
I-	1.02E-03			1.36E-05				1.36E-05		
NO2-	5.86E+01			7.84E-01				7.84E-01		3.75E-03
NO3-	9.72E+02			1.30E+01				1.30E+01		
OH-	5.49E+03			7.31E+01				7.31E+01		
RO4-3	1.45E+02			1.94E+00				1.94E+00		
SO4-2	4.11E+01			5.47E-01				5.47E-01		
TeO4-	8.53E-01			1.14E-02				1.14E-02		
H2O										
MOL										
Organic Carbon	8.19E+01			1.09E+00				1.09E+00		7.36E-01
ZnO2.2H2O	1.17E+03			1.56E+01				1.56E+01		
Ag2O										1.46E-02
AlFO4										2.58E+02
AlFO3										2.13E+03
AmFO3										7.52E-05
BFO3						7.46E+00		7.46E+00		9.32E+02
BFO										3.69E-02
BFO2										3.37E-01
BFO3										7.45E+02
CaO					5.33E-01			5.33E-01		

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Chemicals Continued (MT)										
CaO										3.65E-01
Ca2O3										2.89E-01
Ca2O3										3.47E-09
Ca2O3										1.14E-04
Ca2O3										1.22E+01
Ca2O										3.56E-03
CaO										2.94E-03
Fe2O3										1.08E+00
Fe										2.73E-03
H2O										1.16E-06
K2O										1.96E+01
La2O3										2.23E-02
Li2O					2.66E+00			2.66E+00		1.12E-01
MgO					5.33E-01			5.33E-01		2.35E-02
MnO										2.63E-06
Mn2O3										1.36E-05
Na2O										3.72E+03
Ni2O3										4.67E-01
Rb2O										3.60E-01
R2O2										1.20E-03
Rb2O										1.11E-05
Rh2O3										2.03E-05
SrO										2.46E-03
SiO2					3.73E+01			3.73E+01		1.08E+04
SiO										5.46E+00
SnO										4.17E-02
Ta2O7										6.44E-02
TiO2										1.55E-03
UD3										3.72E+00
ZnO										2.39E-04
ZrO2										7.53E-01
Cement										
Flyash										
Polyelectrolyte	1.34E+02			1.32E+00				1.32E+00		
CS-100 - Na Form					6.20E+02			6.20E+02		

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
LIQUID COMPONENTS										
Total Mass Flow (MT)	9.72E+05	1.16E+04	4.44E+05	4.23E+06		4.80E+05	4.10E+06	1.63E+05	1.77E+04	3.34E+05
Volume (L)	9.72E+08	1.16E+07	3.11E+08	4.23E+09		4.80E+08	4.09E+09	1.59E+08	1.77E+07	3.23E+08
Specific Gravity	1.02E+00	1.03E+00	1.43E+00	1.03E+00		1.00E+00	1.02E+00	1.04E+00	1.00E+00	1.04E+00
Radionuclides (Ci)										
Am-241	1.11E-03	1.11E-06	4.76E+03						1.53E-06	
C-14	6.68E-04	6.69E-07	2.87E+03				2.90E+03		9.21E-07	
Cs-137	2.13E-01	2.13E-04	9.24E+05				3.40E+05		1.16E-02	3.40E+05
Ba-137	2.04E-01	2.04E-04	8.78E+05				3.23E+05		1.10E-02	3.23E+05
Np-237	6.51E-04	6.52E-07	2.80E+03				2.80E+03		6.53E-07	2.79E+03
Ru-239	2.70E-04	2.70E-07	1.16E+03						3.72E-07	
Ru-240	7.43E-05	7.43E-08	3.19E+02						1.02E-07	
Ru-241	9.47E-04	9.48E-07	4.07E+03						1.30E-06	
Sr-90	1.65E-01	1.65E-04	7.10E+05						2.28E-04	
Y-90	1.65E-01	1.65E-04	7.10E+05						2.28E-04	
Tc-99	7.63E-03	7.63E-06	3.29E+04				1.65E+04		9.10E-06	1.65E+04
Total Curies	7.61E-01	7.62E-04	3.27E+06				6.86E+05		2.31E-02	6.83E+05
Chemicals (MT)										
Ag+	7.34E-08	7.33E-11	3.16E-01						1.01E-10	
Am#3	3.23E-10	3.23E-13	1.39E-03						4.45E-13	
As#5										
B#3	4.03E-09	4.04E-12	1.73E-02						5.56E-12	
Bar#2	1.82E-07	1.82E-10	7.82E-01						2.51E-10	
Be#2										
Bi#3	8.76E-07	8.77E-10	3.77E+00						1.21E-09	
Ca#2	3.71E-04	3.71E-07	1.59E+03						3.73E-07	1.59E+03
Cl#2	2.68E-06	2.68E-09	1.15E+01				3.95E+00		3.34E-09	3.95E+00
Co#3	5.46E-07	5.46E-10	2.35E+00						7.51E-10	
Cr#3	3.39E-10	3.40E-13	1.46E-03						4.67E-13	
Cs+	2.77E-08	2.77E-11	1.19E-01				4.15E-02		1.54E-09	4.15E-02
Cl#2	1.29E-08	1.30E-11	5.56E-02						1.78E-11	
Fe#3	2.10E-06	2.11E-09	9.04E+00						2.90E-09	
H+							2.12E+02	1.90E+02	1.78E-01	2.78E+02
Hg#2	3.45E-10	3.46E-13	1.48E-03						4.76E-13	
K+	9.10E-05	9.11E-08	3.91E+02				5.29E+00		1.26E-07	5.29E+00
La#3	4.07E-08	4.08E-11	1.75E-01						5.61E-11	
Mg#2										
Mn#2	1.13E-11	1.13E-14	4.84E-05						1.55E-14	
Mn#4	2.03E-06	2.03E-09	8.71E+00						2.79E-09	
Mo#6	2.74E-12	2.74E-15	1.18E-05				1.18E-05		2.74E-15	1.18E-05
Ne+	4.45E-02	4.46E-05	6.64E+04	6.64E-01			8.99E+02	3.01E+02	6.99E-05	8.99E+02
Ni#3	1.21E-06	1.21E-09	5.21E+00						1.67E-09	
Ni#4	9.24E-07	9.25E-10	3.97E+00				3.97E+00		9.26E-10	3.96E+00
H#4	2.53E-06	2.53E-09	1.09E+01				3.84E+00		3.13E-09	3.84E+00
Ru#4	4.69E-09	4.70E-12	2.02E-02						6.46E-12	
Rb+	5.58E-11	5.58E-14	2.40E-04						7.69E-14	
Rer#7										
Rn#3										
Ru#3										
Se#6	4.39E-09	4.39E-12	1.89E-02				1.89E-02		4.39E-12	1.89E-02
Si#4	3.17E-05	3.17E-08	1.34E+02						4.36E-08	
Sl#2	8.47E-08	8.47E-11	3.64E-01						1.17E-10	
Te#6										
UO2#2	1.46E-05	1.46E-08	6.23E+01						2.01E-08	
Zn#2										
Al(CH)4-	2.16E-03	2.16E-06	9.29E+03						2.98E-06	
NO2-	8.96E-05	8.97E-08	3.85E+02				3.85E+02		8.97E-08	3.85E+02
Cl-	1.09E-03	1.10E-06	2.35E+03				2.24E+03		1.22E-06	1.87E+03
ODS-2									1.26E-07	
Cr(CH)4-	1.10E-04	1.11E-07	4.75E+02						1.52E-07	
F-	6.69E-04	6.69E-07	2.87E+03				2.04E+03		7.60E-07	1.84E+03
I-	2.16E-06	2.16E-09	9.22E+00				9.19E+00		2.17E-09	9.19E+00
NO2-	1.34E-03	1.34E-06	5.74E+03						5.17E-07	
NO3-	5.16E-02	5.17E-05	1.11E+05						1.52E-07	
OH-	2.29E-03	2.29E-06	9.83E+03						1.10E+01	1.10E+01
FO#3	1.40E-03	1.40E-06	6.03E+03				5.17E+02	1.18E+04	3.43E-06	1.34E+02
SO#2	3.75E-04	3.76E-07	1.61E+03	4.91E-01			1.24E+03	2.23E+02	1.82E-06	1.24E+03
TO#4	7.45E-07	7.46E-10	3.20E+00						5.17E-07	
TO#4	7.45E-07	7.46E-10	3.20E+00						8.86E-10	1.61E+00
H2O	9.72E+05	1.08E+04	2.26E+05	5.16E+05		4.80E+05	2.69E+05	8.38E+04	1.67E+04	3.14E+05
Separable Organic	1.11E-16	1.11E-19	4.75E-10						1.11E-19	
Organic Carbon	2.24E-04	2.24E-07	3.36E+02						3.36E-07	
ZnCl2.ZH2O	1.75E-06	1.75E-09	7.51E+00						2.41E-09	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
LIQUID COMPONENTS										
Chemicals Continued (MT)										
Hg	6.89E-14	6.90E-17	2.96E-07				2.62E-03		6.95E-17	2.90E-07
TcO2	1.50E-11	1.50E-14	6.46E-05				1.29E+00		1.50E-14	6.46E-05
Cl2										
CO										
CO2		8.02E+02					3.04E+03		1.06E+03	
F2										
H2										
I2										
N2				2.94E+06			2.96E+06	5.30E+04		
NeO										
NO							1.35E+02			
NCl2							8.25E+02			
O2				7.81E+05			8.32E+05	1.41E+04		
SO2							9.72E+02			
Glycolic Anion	2.79E-14	2.79E-17	1.20E-07						3.81E-17	
H2S										
Glycolic Acid										
Xerosene								1.00E+01		
NEB								1.70E+03		
Polyelectrolyte	3.99E-06	3.99E-09	1.71E+01						5.49E-09	
Sulfur										

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
SOLID COMPONENTS										
Total Mass Flow (MT)			2.00E+04	3.40E+05	4.42E+05	8.98E+03	9.66E+03	6.20E+03		1.01E+04
Radionuclides (Ci)										
Am-241			1.04E+03		5.57E+03	1.13E+02	1.22E+02			1.22E+02
C-14			2.75E+01							
Cs-137			9.76E+04		6.54E+05	1.33E+04	1.43E+04			1.43E+04
Ba-137			9.28E+04		6.21E+05	1.26E+04	1.36E+04			1.36E+04
Np-237			8.63E-01		8.25E-01	1.65E-02	1.80E-02			1.80E-02
Pu-239			3.39E+02		1.44E+03	2.92E+01	3.14E+01			3.14E+01
Pu-240			9.94E+01		4.02E+02	8.16E+00	8.78E+00			8.78E+00
Pu-241			1.12E+03		4.98E+03	1.01E+02	1.09E+02			1.09E+02
Sr-90			6.16E+05		1.27E+06	2.58E+04	2.78E+04			2.78E+04
Y-90			6.16E+05		1.27E+06	2.58E+04	2.78E+04			2.78E+04
Tc-99			8.13E+02		1.65E+04	3.35E+02	3.61E+02			3.61E+02
Total Curies			1.43E+06		3.85E+06	7.82E+04	8.41E+04			8.41E+04
Chemicals (MT)										
Ag+			7.31E-03							
Al+3			1.25E+01							
Am+3			2.34E-04							
As+5										
Be+2										
Be+2										
Bi+3			3.40E+00							
Bi+3			3.19E+02					1.80E+03		3.17E+02
Cl-2			3.11E-02							
Ce+3			3.09E+00							
Cl-3			7.51E-08							
Co+3			4.70E-04							
Co+3			1.68E+00							
Cs+			2.32E-03							
Cr+2										
Fe+3			8.93E+00							
Fe+2			1.16E-03							
K+			3.58E-01							
La+3			2.79E-01							
Mg+2			1.47E-02							
Mn+4			2.32E+00							
Mn+6			2.15E-04							
Na+			2.18E+01							
Ni+3			2.64E+00							
Np+4			1.22E-03		1.17E-03	2.38E-05	2.56E-05			2.56E-05
Pb+4			3.49E-01							
Pu+4			4.66E-03							
Rn+3			3.92E-04							
Se+6			3.62E-02							
Si+4			6.23E+00							
Sn+2			4.73E-01							
Ti+4			3.32E-02							
Ti+4										
UO2+2			2.07E+01							
Zn+2			4.55E-03							
Cl-			4.88E+00		1.13E+02	2.30E+00	2.47E+00			2.47E+00
CO3-2			1.22E+00							
F-			1.92E+02		9.83E+02	2.00E+01	2.15E+01			1.71E+02
I-			3.77E-03		8.90E-02	1.81E-03	1.95E-03			1.95E-03
NO2-			7.84E-01							
NO3-			1.30E+01							
OH-			7.31E+01							
PO4-3			1.94E+00					1.53E+03		
SO4-2			5.47E-01							
ToO4-			1.14E-02							
H2O										
W6O2			7.36E-01		1.75E+01	3.55E-01	3.81E-01			3.81E-01
Organic Carbon			1.09E+00							
ZnO2.2H2O			1.56E+01							
Ag2O			1.46E-02		3.47E-01	7.05E-03	7.58E-03			7.58E-03
Al(OH)3			2.58E+02		6.11E+03	1.24E+02	1.34E+02			1.34E+02
Al2O3			2.13E+03	4.80E+04	5.05E+04	1.03E+03	1.10E+03			1.10E+03
Am2O3			7.52E-05		1.78E-03	3.62E-05	3.90E-05			3.90E-05
B2O3			9.39E+02	2.21E+04	2.21E+04	4.49E+02	4.83E+02			4.83E+02
B2O			3.68E-02		8.73E-01	1.77E-02	1.91E-02			1.91E-02
Bi2O3			3.37E-01		7.98E+00	1.62E-01	1.75E-01			1.75E-01
CaO			7.46E+02	1.50E+04	1.77E+04	3.59E+02	3.86E+02			3.86E+02

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
SOLID COMPONENTS										
Chemicals Continued (MT)										
Cd			3.65E-01		8.67E+00	1.76E-01	1.89E-01			1.89E-01
Ca2O3			2.69E-01		6.38E+00	1.30E-01	1.39E-01			1.39E-01
Ca2O			3.47E-09		8.24E-08	1.67E-09	1.80E-09			1.80E-09
Co2O3			1.14E-04		2.71E-03	5.51E-05	5.93E-05			5.93E-05
Cr2O3			1.23E+01		3.03E+02	6.15E+00	6.62E+00			6.62E+00
Ca2O			3.56E-03		8.43E-02	1.71E-03	1.84E-03			1.84E-03
CrO			2.94E-03		6.96E-02	1.41E-03	1.32E-03			1.32E-03
Fe2O3			1.02E+00		2.57E+01	5.22E-01	5.62E-01			5.62E-01
Hg			2.73E-03		2.62E-03	5.32E-05	5.72E-05			2.67E-03
HgO			1.16E-06		2.74E-05	5.56E-07	5.99E-07			5.98E-07
K2O			1.98E+01		4.65E+02	9.45E+00	1.02E+01			1.02E+01
La2O3			2.23E-02		5.33E-01	1.08E-02	1.17E-02			1.17E-02
Li2O			2.78E+00		2.66E+00	5.41E-02	5.82E-02			5.82E-02
MgO			5.56E-01		5.57E-01	1.13E-02	1.22E-02			1.22E-02
MnO			2.63E-06		6.25E-05	1.27E-06	1.37E-06			1.37E-06
Mn2O3			1.34E-05		3.22E-04	6.54E-06	7.04E-06			7.04E-06
Na2O			3.73E+03		8.84E+04	1.80E+03	1.93E+03			1.93E+03
Ni2O3			4.67E-01		1.11E+01	2.25E-01	2.42E-01			2.42E-01
NiO			3.60E-01		8.53E+00	1.73E-01	1.86E-01			1.86E-01
PbO			1.20E-03		2.94E-02	5.78E-04	6.20E-04			6.20E-04
Pb2O			1.11E-05		2.62E-04	5.33E-06	5.73E-06			5.73E-06
Pb2O3			2.03E-05		4.80E-04	9.76E-06	1.05E-05			1.05E-05
SnO			2.44E-03		5.83E-02	1.18E-03	1.27E-03			1.27E-03
SiO2			1.08E+04	2.55E+05	2.53E+05	5.18E+03	5.57E+03			5.57E+03
SiO			5.46E+00		1.30E+02	2.63E+00	2.83E+00			2.83E+00
SrO			4.17E-02		9.88E-01	2.01E-02	2.16E-02			2.16E-02
Ti2O7			6.44E-02		1.53E+00	3.10E-02	3.34E-02			3.34E-02
TiO2			1.59E-05		3.77E-02	7.67E-04	8.25E-04			8.25E-04
UO			3.72E+00		8.82E+01	1.79E+00	1.93E+00			1.93E+00
ZnO			2.39E+04		5.67E-03	1.15E-04	1.24E-04			1.24E-04
ZrO			7.53E-01		1.79E+01	3.63E-01	3.90E-01			3.90E-01
Cement								1.44E+03		
Flyash								1.44E+03		
Polyelectrolyte			1.32E+00							
CS-100 - Na Form			6.20E+02							

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
LIQUID COMPONENTS										
Total Mass Flow (MT)	3.95E+06	4.08E+02			7.31E+02	1.83E+03	1.36E+05	1.51E+03	3.42E+04	8.13E+03
Volume (L)	3.95E+09	4.08E+05			7.31E+05	1.83E+06	1.36E+08	1.51E+06	3.31E+07	8.13E+06
Specific Gravity	1.02E+00	1.02E+00			1.02E+00	1.02E+00	1.02E+00	1.02E+00	1.03E+00	1.03E+00
Radionuclides (Ci)										
Am-241	1.53E-06					4.64E-04	3.93E-06	3.94E-09	9.38E+00	
C-14	2.90E+03					2.80E-04	2.37E-06	2.37E-09	5.63E+00	
Cs-137	1.33E-02					6.64E+02	5.94E-02	5.33E-05	1.27E+05	
Ba-137	1.27E-02					6.30E+02	5.08E-02	5.08E-05	1.21E+05	
Np-237	1.46E-05					6.66E-07	5.44E-09	5.45E-12	1.30E-02	
Pu-239	3.72E-07					1.13E-04	9.58E-07	9.59E-10	2.28E+00	
Pu-240	1.02E-07					3.11E-05	2.63E-07	2.64E-10	6.28E-01	
Pu-241	1.30E-06					3.97E-04	3.36E-06	3.36E-09	8.01E+00	
Sr-90	2.28E-04					6.92E-02	5.86E-04	5.87E-07	1.40E+03	
Y-90	2.28E-04					6.92E-02	5.86E-04	5.87E-07	1.40E+03	
Tc-99	9.16E-05					4.36E-01	1.37E-05	1.37E-08	3.27E+01	
Total Curies	3.48E+03					1.29E+03	1.05E-01	1.06E-04	2.51E+05	
Chemicals (MT)										
Ag+	1.01E-10					3.08E-08	2.61E-10	2.61E-13	6.21E-04	
AmF3	4.45E-13					1.35E-10	1.15E-12	1.15E-15	2.73E-06	
AsF5										
BH3	5.56E-12					1.69E-09	1.43E-11	1.43E-14	3.41E-05	
BaF2	2.51E-10					7.62E-08	6.46E-10	6.46E-13	1.54E-03	
BeF2										
Rn3	1.21E-09				1.27E-10	8.49E-07	7.19E-09	7.20E-12	1.72E-02	
CaF2	3.73E-07					2.96E-06	2.51E-08	2.51E-11	5.98E-02	
CH2	2.31E-08					7.36E-07	6.24E-09	6.24E-12	1.49E-02	
CrF3	7.55E-10					2.29E-07	1.94E-09	1.95E-12	4.63E-03	
CrF3										
CuF3	4.67E-13					1.42E-10	1.20E-12	1.20E-15	2.87E-06	
Cu+	1.75E-09					8.75E-05	2.93E-09	2.94E-12	6.99E-03	
ClF2	1.78E-11					5.42E-09	4.59E-11	4.60E-14	1.10E-04	
FeF5	2.90E-09					1.73E-06	1.46E-08	1.46E-11	3.48E-02	
H+	1.78E-01					2.12E-05				
HgF2	4.76E-13					1.45E-10	1.22E-12	1.23E-15	2.92E-06	
K+	1.53E-07					1.16E-04	3.20E-07	3.20E-10	7.62E-01	
LaF3	5.61E-11					1.71E-08	1.45E-10	1.45E-13	3.65E-04	
MgF2										
MnF2	1.55E-14					4.71E-12	3.99E-14	4.00E-17	9.52E-08	
MnF4	2.79E-09					8.49E-07	7.19E-09	7.20E-12	1.72E-02	
MoF6	6.16E-14							1.18E-22	2.82E-13	
Na+	7.44E-05				8.24E-06	5.49E-02	3.71E-04	3.71E-07	6.67E+02	
NiF3	1.67E-09					5.08E-07	4.30E-09	4.30E-12	1.03E-02	
NpF4	2.08E-08					9.45E-10	7.72E-12	7.72E-15	1.84E-05	
HF4	2.24E-08					6.86E-07	5.81E-09	5.82E-12	1.39E-02	
PuF4	6.46E-12					1.96E-09	1.66E-11	1.67E-14	3.97E-05	
Rb+	7.69E-14					2.34E-11	1.98E-13	1.98E-16	4.72E-07	
RbF7										
RnF3										
RnF3										
SbF6	9.87E-11					2.23E-14	1.89E-16	1.89E-19	4.51E-10	
SiF4	4.36E-08					5.71E-05	4.84E-07	4.84E-10	1.15E+00	
SnF2	1.17E-10					3.55E-08	3.00E-10	3.01E-13	7.16E-04	
TaF6										
UF2F2	2.01E-08					2.60E-05	2.20E-07	2.21E-10	5.26E-01	
ZnF2										
Al(OH)3	2.98E-06					4.00E-03	3.39E-05	3.40E-08	8.09E+01	
B2	2.01E-06					4.50E-10	3.86E-12	3.86E-15	9.21E-06	
Cl-	1.24E-05				9.97E-06	4.66E-05	7.89E-07	7.90E-10	9.41E-01	
CO3-2	1.26E-07					1.07E-09	1.19E-06	1.19E-09	6.84E+00	
Cr(OH)3	1.52E-07					6.65E-05	5.63E-07	5.64E-10	1.34E+00	
F-	1.10E-05					1.01E-04	8.54E-07	8.55E-10	2.04E+00	
I-	4.81E-08					8.75E-09	7.41E-11	7.42E-14	1.77E-04	
NO2-	1.84E-06					2.18E-03	3.69E-05	3.70E-08	8.81E+01	
NO3-	1.10E+01					6.77E-02	1.64E-04	1.64E-07	1.95E+02	
OH-	3.46E-06				2.12E-08	1.45E-07	1.61E-04	1.62E-07	3.85E+02	
PO4-3	8.02E-06				1.30E-06	6.78E-05	5.72E-06	5.73E-09	1.36E+01	
SO4-2	5.17E-07					4.01E-04	1.33E-06	1.33E-09	3.18E+00	
ToD4-	8.86E-10					4.25E-05	1.34E-09	1.34E-12	3.18E-03	
HD	5.69E+04					1.83E+03	1.36E+05	1.51E+03	3.27E+04	1.70E+03
Separable Organic	1.11E-19					7.59E-06	6.43E-08	6.44E-11	1.53E-04	
Organic Carbon	3.38E-07					2.30E-04	7.94E-07	7.94E-10	6.62E-01	
ZnO2·2H2O	2.41E-09					7.32E-07	6.20E-09	6.21E-12	1.48E-02	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
LIQUID COMPONENTS										
Chemicals Continued (MT)										
Hg	1.53E-08						1.24E-15	1.24E-18	2.96E-09	
TcO2	6.46E-09									
Cl2										
CO	2.04E+01									
CO2	4.10E+03									
F2										
H2	7.09E+01									
I2										
N2	3.02E+06									
N2O										
NO	1.35E+00									
NO2	1.03E+01									
O2	8.65E+05									
SO2	9.72E+01									
Glycollic Anion	3.81E-17					1.39E+00	5.81E-07	5.82E-10	1.39E+00	2.36E+03
H2S	3.22E+01									
Glycollic Acid										4.07E+03
Kerosene										
NE3	1.79E+01									
Polyelectrolyte	5.49E-09					1.04E-04	8.79E-07	8.79E-10	2.09E+00	
Sulfur		4.08E+02								

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
SOLID COMPONENTS										
Total Mass Flow (MT)	2.23E+01		5.75E+03			1.96E+00			1.48E+04	2.51E+04
Radionuclides (Ci)										
Am-241	2.62E-03					2.99E+00			6.03E+04	
C-14						1.02E-01			2.07E+03	
Cs-137	3.31E-01					2.62E+02			5.25E+06	
Ba-137	3.14E-01					2.49E+02			4.99E+06	
Np-237	4.17E-07					3.07E-03			6.19E+01	
Ru-229	7.27E-04					1.04E+00			2.09E+04	
Ru-240	2.03E-04					3.07E-01			6.19E+03	
Pu-241	2.52E-03					3.40E+00			6.86E+04	
Sm-90	6.43E-01					2.09E+03			4.22E+07	
Y-90	6.43E-01					2.09E+03			4.22E+07	
Tc-99	8.34E-03					4.67E-01			8.76E+03	
Total Curies	1.95E+00					4.71E+03			9.48E+07	
Chemicals (MT)										
Ag+						2.72E-05			5.49E-01	
Al+3						4.65E-02			9.39E+02	
Am+3						8.70E-07			1.76E-02	
As+5										
Ba+2										
Ba+2										
Bi+3						1.26E-02			2.53E+02	
Ca+2			1.18E+02			6.33E-03			1.28E+02	
Ca+2						1.16E-04			2.33E+03	
Ca+3						1.15E-02			2.32E+02	
Cl+3						2.79E-10			5.64E-06	
Co+3						1.73E-06			3.53E-02	
Co+3						6.23E-03			1.26E+02	
Cr+						8.60E-06			1.74E-01	
Cr+2										
Fe+3						3.32E-02			6.71E+02	
Hg+2						4.31E-06			8.70E-02	
K+						1.33E-03			2.69E+01	
La+3						1.04E-03			2.10E+01	
Mg+2						5.45E-05			1.10E+00	
Mn+6						8.61E-03			1.74E+02	
Mn+6						7.98E-07			1.61E-02	
Na+			3.01E+02			8.10E-02			1.64E+03	
Ni+3						9.88E-03			2.06E+02	
Np+4	5.91E-10					4.36E-06			8.78E-02	
Pb+4						1.30E-03			2.62E+01	
Pu+4						1.81E-05			3.65E-01	
Rb+3						1.45E-06			2.93E-02	
Se+6						1.35E-04			2.72E+00	
Si+4						2.32E-02			4.68E+02	
Sn+2						1.77E-03			3.57E+01	
Tb+4						1.22E-04			2.49E+00	
Ti+4										
UO2+2						7.69E-02			1.55E+03	
Zn+2						1.69E-05			3.42E-01	
Cl-	5.72E-05		3.65E+02			9.15E-04			8.78E+00	
CO3-2						4.52E-03			9.12E+01	
F-	4.97E-04		5.30E+01			4.46E-03			6.71E+01	
I-	4.50E-08					5.07E-08			1.02E-03	
NO2-						2.91E-03			5.83E+01	
NO3-						4.81E-02			9.72E+02	
OH-						2.47E-01			5.49E+03	
HO4-3						7.20E-03			1.45E+02	
SO4-2						2.03E-03			4.11E+01	
TeO4-						4.22E-05			8.53E-01	
H2O			1.99E+03							
NaCl2	8.82E-06					2.73E-05			2.73E-05	
Organic Carbon						4.06E-03			8.19E+01	
ZrO2·2H2O						5.78E-02			1.17E+03	
Ag2O	4.75E-07					5.86E-08			5.86E-08	
Al(OH)3	3.09E-03					2.03E-05			2.03E-05	
Al2O3	2.55E-02					1.72E-04			1.72E-04	
Am2O3	9.02E-10					1.92E-09			1.92E-09	
B2O3	1.12E-02					2.33E-01			2.33E-01	4.66E+03
B4O7	4.42E-07					1.71E-10			1.71E-10	
Bi2O3	4.04E-06					2.82E-05			2.82E-05	
CaO	8.93E-03					1.78E-05			1.78E-05	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
SOLID COMPONENTS										
Chemicals Continued (MT)										
Cd	4.38E-06					2.16E-05			2.16E-05	
Ca2O3	3.22E-06					2.70E-05			2.70E-05	
Cr2O3	4.16E-14					6.13E-13			6.13E-13	
Cr2O3	1.37E-09					8.14E-09			8.14E-09	
Cr2O3	1.53E-04					1.83E-05			1.83E-05	
Cs2O	4.26E-08					6.93E-06			6.93E-06	
CUO	3.52E-08					1.36E-11			1.36E-11	
Fe2O3	1.33E-05					9.51E-05			9.51E-05	
Hg	1.32E-09									
HgO	1.38E-11									
K2O	2.33E-04					5.76E-06			5.76E-06	
La2O3	2.69E-07					2.44E-06			2.44E-06	
Li2O	1.33E-06					1.83E-02			1.83E-02	3.70E+02
MgO	2.82E-07					1.81E-07			1.81E-07	
MnO	3.16E-11					1.22E-14			1.22E-14	
MoO3	1.63E-10					1.21E-08			1.21E-08	
Na2O	4.47E-02					6.07E-04			6.07E-04	
Ni2O3	5.60E-06					2.79E-05			2.79E-05	
NO2	4.31E-06					1.66E-04			1.66E-04	
NO2	1.43E-08					4.10E-08			4.10E-08	
Re2O	1.33E-10					5.12E-14			5.12E-14	
Rb2O3	2.43E-10					3.58E-09			3.58E-09	
SeO3	2.93E-06					2.41E-05			2.41E-05	
SiO2	1.29E-01					9.96E-01			9.96E-01	2.01E+04
SO3	6.55E-05					2.03E-06			2.03E-06	
SiO	5.00E-07					4.17E-06			4.17E-06	
Ti2O7	7.72E-07					3.08E-06			3.08E-06	
ThO2	1.91E-08					2.81E-07			2.81E-07	
UO3	4.46E-05					1.63E-04			1.63E-04	
ZnO	2.87E-09					4.22E-08			4.22E-08	
ZrO2	9.03E-06					8.97E-05			8.97E-05	
Cement			1.44E+03							
Flyash			1.44E+03							
Polyelectrolyte						6.61E-03				
CS-100 - Na Foam									1.34E+02	

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
LIQUID COMPONENTS								
Total Mass Flow (MT)	1.60E+04		7.07E+04	1.16E+01	4.73E+04	7.11E+03	8.22E-02	1.12E+06
Volume (L)	1.59E+07		7.07E+07	1.16E+04	4.73E+07	7.11E+06	8.22E+01	1.12E+09
Specific Gravity	1.00E+00		1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00
Radionuclides (Ci)								
Am-241			4.69E-04			4.69E-06		1.06E-03
C-14			2.07E+03			2.07E+03		6.37E-04
Cs-137			6.70E+02			6.70E+00		1.02E+00
Ba-137			6.37E+02			6.37E+00		9.73E-01
Np-237	4.62E-04		1.35E-02		1.44E-10	8.57E-06		3.06E-04
Pu-239			1.14E-04			1.14E-06		2.57E-04
Pu-240			3.14E-05			3.14E-07		7.08E-05
Pu-241			4.01E-04			4.01E-06		9.03E-04
Sr-90			6.99E-02			6.99E-04		1.58E-01
Y-90			6.99E-02			6.99E-04		1.58E-01
Tc-99	8.78E+03		8.78E+03		2.63E-03	5.60E+00		8.11E-03
Total Curies	8.78E+03		1.26E+04		2.63E-03	2.51E+03		2.32E+00
Chemicals (MT)								
Ag+			3.11E-08			3.11E-10		7.00E-08
Am+3			1.37E-10			1.37E-12		3.08E-10
As+5								
BH3			1.71E-09			1.71E-11		3.85E-09
Ba+2			7.70E-08			7.70E-10		1.74E-07
Be+2								
Bi+3			8.57E-07			8.57E-09		8.38E-07
Ca+2			2.99E-06			2.99E-08		2.57E-04
CaH2			7.44E-07			7.44E-09		2.31E-06
Ca+3			2.32E-07			2.32E-09		5.22E-07
Cr+3								
Co+3			1.43E-10			1.43E-12		3.23E-10
Cs+			8.83E-05			8.83E-07		1.32E-07
Cl+2			5.48E-09			5.48E-11		1.23E-08
Fe+3	4.28E-01		1.74E-06	9.05E-06	1.28E-07	1.74E-08		2.01E-06
H+			2.14E-05			2.59E-04		
Hg+2			1.46E-10			1.46E-12		3.29E-10
K+			1.17E-04			1.17E-06		8.65E-05
La+3			1.72E-08			1.72E-10		3.88E-08
Mg+2								
Mn+2			4.76E-12			4.76E-14		1.07E-11
Mn+4			8.57E-07			8.57E-09		1.93E-06
Mo+6								
Na+			5.55E-02			5.55E-04		4.84E-02
Ni+3			5.13E-07			5.13E-09		1.16E-06
Np+4	6.83E-07		1.91E-05		2.05E-13	1.22E-08		4.34E-07
Pr+4			6.93E-07			6.93E-09		2.18E-06
Pu+4			1.98E-09			1.98E-11		4.47E-09
Rb+			2.36E-11			2.36E-13		5.32E-11
Ra+7								
Rn+3								
Ru+3								
Se+6			2.25E-14			2.25E-16		3.03E-09
Si+4			5.77E-05			5.77E-07		3.03E-05
Sn+2			3.58E-08			3.58E-10		8.07E-08
Ta+6								
UO2+2			2.63E-05			2.63E-07		1.40E-05
Zn+2								
Al(OH)4-			4.05E-03			4.05E-05		2.08E-03
BrO2-			4.60E-10			4.60E-12		6.19E-05
Cl-			4.70E-05			4.70E-07		8.51E-04
ClO2-						1.19E-10		8.80E-05
Cr(OH)4-			6.72E-05			6.72E-07		1.05E-04
I-			1.02E-04			1.02E-06		5.25E-04
NO2-			8.94E-09			8.94E-11		1.47E-06
NCO-			2.20E-03			2.20E-05		1.30E-03
NCO-	1.87E+01		6.84E-02	5.61E-04	1.12E-05	1.26E-02		5.38E-02
OH-						1.62E-08		2.50E-03
PO4-3			6.82E-04			6.82E-06		1.22E-03
SO4-2	4.92E+00		4.05E-04		1.48E-06	3.14E-03		3.59E-04
ToO4-	8.53E-01		4.29E-05		2.56E-07	4.29E-07		7.89E-07
H2O	1.59E+04		6.39E+04	1.16E+01	4.73E+04	3.77E+02		1.12E+06
Separable Organic			7.66E-06			7.67E-08		4.84E-08
Organic Carbon			2.32E-04			2.32E-06		2.34E-04
ZnO2.ZR2O			7.39E-07			7.39E-09		1.67E-06

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
LIQUID COMPONENTS								
Chemicals Continued (MT)								
Hg	9.61E-02		1.83E-01		2.88E-08	1.25E-03	8.22E-02	1.99E-08
Toc2			6.87E-01			4.37E-04		1.04E-11
CL2			1.94E-02			1.94E-02		
Cl								
CO2			5.46E+03			5.46E+03		
F2			9.22E-02			9.22E-02		
H2								
I2			1.20E-03			1.20E-03		
N2			1.35E+02			1.35E+02		
N2O			1.40E+01			1.40E+01		
NO			9.14E+02			9.05E+02		
NO2								
O2			2.15E+02			2.07E+02		
SO2			1.64E+01			1.31E+01		
Glycolic Anion			1.40E+00			1.40E-02		4.02E-07
H2S								
Glycolic Acid								
Kerosene								
NE			2.72E+00			2.72E+00		
Polyelectrolyte			1.03E-04			1.03E-06		4.39E-06
Sulfur								

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
SOLID COMPONENTS								
Total Mass Flow (MT)	1.54E+02	3.70E+04	1.56E+02			2.94E-08		
Radionuclides (Ci)								
Am-241	1.21E+02	6.03E+04	1.24E+02			2.64E-08		
C-14	1.03E-03		1.03E-01			2.59E-10		
Cs-137	3.74E+04	1.87E+07	3.77E+04			6.61E-06		
Ba-137	3.55E+04	1.77E+07	3.58E+04			6.28E-06		
Np-237	1.24E-01	6.19E+01	1.27E-01			2.75E-11		
Pu-239	4.19E+01	2.09E+04	4.25E+01			9.22E-09		
Pu-240	1.24E+01	6.19E+03	1.27E+01			2.75E-09		
Pu-241	1.38E+02	6.86E+04	1.41E+02			3.05E-08		
Sm-90	8.46E+04	4.22E+07	8.67E+04			1.37E-05		
Y-90	8.46E+04	4.22E+07	8.67E+04			1.87E-05		
Tc-99	6.71E+02	8.78E+03	6.72E+02			1.08E-07		
Total Corries	2.43E+05	1.21E+08	2.48E+05			5.06E-05		
Chemicals (MT)								
Ag+	2.75E-07		2.75E-05			6.86E-14		
Al+3	4.70E-04		4.70E-02			1.17E-10		
Am+3	8.78E-09		8.78E-07			2.20E-15		
As+5								
Be+2								
Be+2								
Bi+3	1.28E-04		1.28E-02			3.19E-11		
Ca+2	6.39E-05		6.39E-03			1.60E-11		
Ca+2	1.17E-06		1.17E-04			2.92E-13		
Ce+3	1.16E-04		1.16E-02			2.90E-11		
Cr+3	2.82E-12		2.82E-10			7.05E-19		
Cr+3	1.77E-08		1.77E-06			4.41E-15		
Cu+3	6.30E-05		6.30E-03			1.57E-11		
Ca+	8.69E-08		8.69E-06			2.17E-14		
O+2								
Fe+3	3.35E-04		3.35E-02			8.38E-11		
Fe+2	4.35E-08		4.35E-06			1.09E-14		
K+	1.34E-05		1.34E-03			3.36E-12		
La+3	1.05E-05		1.05E-03			2.62E-12		
Mg+2	5.50E-07		5.50E-05			1.38E-13		
Mn+4	8.70E-05		8.70E-03			2.17E-11		
Mn+6	8.06E-09		8.06E-07			2.01E-15		
Ni+	8.18E-04		8.18E-02			2.05E-10		
Ni+3	9.98E-05		9.98E-03			2.49E-11		
Np+4	1.76E-04	8.78E-02	1.80E-04			3.90E-14		
Pb+4	1.31E-05		1.31E-03			3.27E-12		
Pu+4	1.62E-07		1.62E-05			4.56E-14		
Rn+3	1.46E-08		1.46E-06			3.66E-15		
Se+6	1.36E-06		1.36E-04			3.40E-13		
Si+4	2.34E-04		2.34E-02			5.85E-11		
Si+2	1.78E-05		1.78E-03			4.46E-12		
Th+4	1.23E-06		1.23E-04			3.11E-13		
Ti+4								
UO2+2	7.77E-04		7.77E-02			1.94E-10		
Zn+2	1.72E-07		1.72E-05			4.27E-14		
Cl-	9.70E+00	9.70E+00	9.70E+00			1.35E-09		
CO3-2	4.56E-05		4.56E-03			1.14E-11		
F-	2.30E+01	6.91E+01	2.30E+01			3.67E-09		
I-	5.12E-10		5.12E-08			1.28E-16		
NO2-	2.94E-05		2.94E-03			7.35E-12		
NO3-	4.86E-04		4.86E-02			1.22E-10		
OH-	2.50E-03		2.50E-01			6.25E-10		
PO4-3	7.27E-05		7.27E-03			1.82E-11		
SO4-2	2.06E-05		2.06E-03			5.14E-12		
ToC+	4.26E-07		4.26E-05			1.07E-13		
H2O								
H2O2	5.52E-01	2.75E+02	5.52E-01			8.79E-11		
Organic Carbon	4.10E-05		4.10E-03			1.02E-11		
ZnO2.2H2O	5.84E-04		5.84E-02			1.46E-10		
Ag2O	1.15E-03	5.91E-01	1.15E-03			1.88E-13		
Al(OH)3	4.09E-01	2.04E+02	4.09E-01			6.50E-09		
Al2O3	3.47E+00	1.73E+03	3.47E+00			5.53E-10		
Am2O3	3.87E-05	1.93E-02	3.87E-05			6.16E-15		
B2O3	4.70E+01	4.66E+03	4.70E+01			8.07E-09		
B4O	3.45E-06	1.72E-03	3.45E-06			5.49E-16		
Bi2O3	5.70E-01	2.84E+02	5.70E-01			9.07E-11		
CaO	3.59E-01	1.79E+02	3.59E-01			5.71E-11		

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Table 13 Phase 2 Mass Balance with TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
SOLID COMPONENTS								
Chemicals Continued (MT)								
CaO	4.37E-01	2.69E+00	4.37E-01			6.96E-11		
Ca ₂ O ₃	5.44E-01	2.72E+02	5.44E-01			8.67E-11		
Ca ₃ O ₃	1.24E-08	6.18E-06	1.24E-08			1.97E-18		
Ca ₃ O ₂	1.63E-04	4.97E-02	1.63E-04			2.62E-14		
Ca ₃ O	3.70E-01	1.85E+02	3.71E-01			5.90E-11		
Ca ₂ O	1.40E-01	2.05E+00	1.40E-01			2.23E-11		
CaO	2.75E-07	1.37E-04	2.75E-07			4.37E-17		
Fe ₂ O ₃	1.92E+00	9.59E+02	1.92E+00			3.06E-10		
Fe								
H ₂ O								
K ₂ O	1.16E-01	3.52E+01	1.17E-01			1.85E-11		
La ₂ O ₃	4.93E-02	2.44E+01	4.93E-02			7.85E-12		
Li ₂ O	7.41E-01	3.70E+02	7.59E-01			1.64E-10		
MgO	3.66E-03	1.82E+00	3.66E-03			5.82E-13		
MnO	2.46E-10	1.23E-07	2.46E-10			3.92E-20		
Na ₂ O	2.44E-04	2.42E-02	2.44E-04			3.89E-14		
Na ₂ O	1.23E+01	3.70E+03	1.23E+01			1.95E-09		
Ni ₂ O ₃	5.63E-01	2.81E+02	5.63E-01			8.97E-11		
Na ₂ O	3.36E+00	3.02E+01	3.36E+00			5.35E-10		
Na ₂ O	8.29E-04	4.14E-01	8.29E-04			1.32E-13		
Na ₂ O	1.03E-09	5.16E-07	1.03E-09			1.65E-19		
Na ₂ O ₃	7.23E-05	3.61E-02	7.23E-05			1.15E-14		
Na ₂ O	4.86E-01	4.37E+00	4.86E-01			7.74E-11		
SiO ₂	4.22E+01	2.11E+04	4.22E+01			9.23E-09		
SiO ₃	4.10E-02	2.05E+01	4.10E-02			6.54E-12		
SiO	8.42E-02	4.20E+01	8.42E-02			1.34E-11		
Ti ₂ O ₃	6.22E-02	8.13E-01	6.22E-02			9.90E-12		
TiO ₂	5.68E-03	2.83E+00	5.68E-03			9.04E-13		
UO ₃	3.30E+00	1.65E+03	3.30E+00			5.26E-10		
ZnO	8.53E-04	4.26E-01	8.53E-04			1.36E-13		
Zn ₂ O	1.81E+00	9.04E+02	1.81E+00			2.88E-10		
Cement								
Flyash								
Polyelectrolyte	6.68E-05		6.68E-03			1.67E-11		
CS-100 - Na Form								

The pretreatment facilities are scheduled to begin operations in the year 2011. Implementation of the Phase 2 pretreatment operation requires that sufficient tank space has been freed to receive retrieved sludges into the 241-AN, -AW and -AP tank farms. The space is made available by evaporating dilute waste, and by processing some of the DST wastes during Phase 1.

The following text describes the operation of an in-tank sludge treatment operation that accomplishes multiple stages of washing (initial wash concurrent with retrieval, followed by an enhanced caustic wash, followed by three dilute caustic washes), and three stages of blending to arrive at treated sludges that are suitable for vitrification.

3.2.1 Settle and Decant

Figure 15 depicts an operating scenario¹³ utilizing DSTs to perform the functions of settling, decanting, leaching, washing, accumulating, and staging pretreated waste to subsequent out-of-tank pretreatment operations for supernates, or to vitrification for pretreated HLW solids. Figure 16 depicts a DST modified and equipped for in-tank sludge washing. Each washing tank is equipped with a floating suction decant pump, a transfer pump, and two or more mixing pumps. The waste inlet lines extend to near the bottom of the tank to facilitate settling.

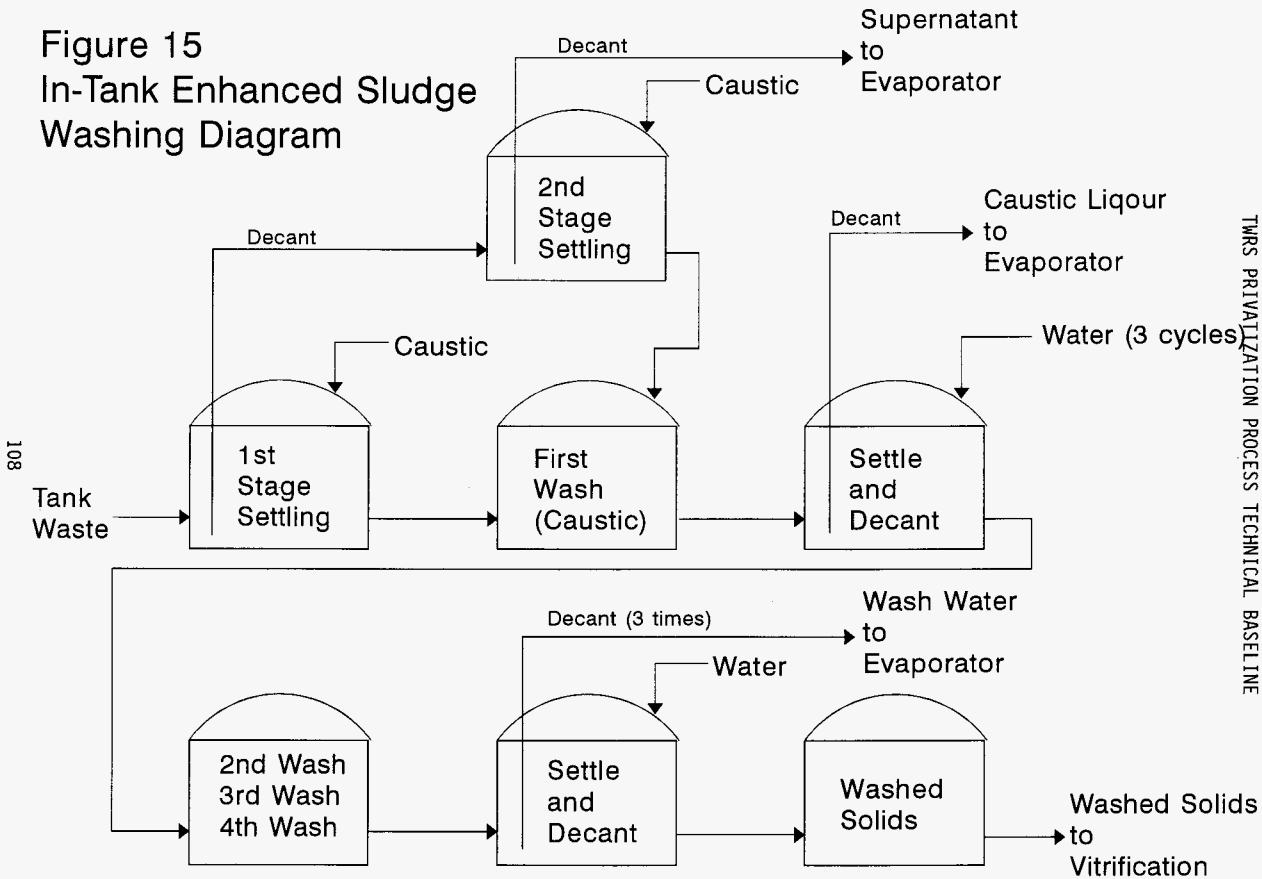
Retrieved slurry is transferred to a first-stage settling tank. The retrieved slurries are on the average 3 wt% solids, although wide variations in solids loading can be expected in actual practice. In the first stage settling tank, the slurries settle to a solids layer containing 20 wt% solids. The operation of the several first-stage tanks is staggered so that each tank is at a different point in the settling process. After a one-month settling period¹⁴, the supernatant is decanted by the floating suction decant pump to one of the second-stage settling tanks. On the average, a cumulative 13.7 million liters of retrieved slurry will be processed through a settling tank, to accumulate 1.3 million liters of settled solids before the settled solids are washed with caustic, and 12.4 million liters will be decanted. The cycle for transferring, settling and decanting waste requires 45 days. On the average, each first-stage tank is capable of accumulating a 1.3 million-liter batch of solids in approximately 6 to 7.5 months (4 to 5 settling cycles).

Decantation of supernatants from first-stage settling tanks is expected to entrain some solids. The supernatants will be allowed to settle for 1 month in the second-stage settling tanks. When second-stage settling is complete, the supernatants are decanted to supernatant accumulation tanks. Small volumes of solids can be expected to accumulate in the second-stage settling tanks over long periods of time. Accumulations of solids in the second-stage settling tanks are transferred out to the first-wash tank as required.

¹³Sludge washing can be performed in one tank; the diagram depicts the steps in the process, not necessarily the required number of tanks.

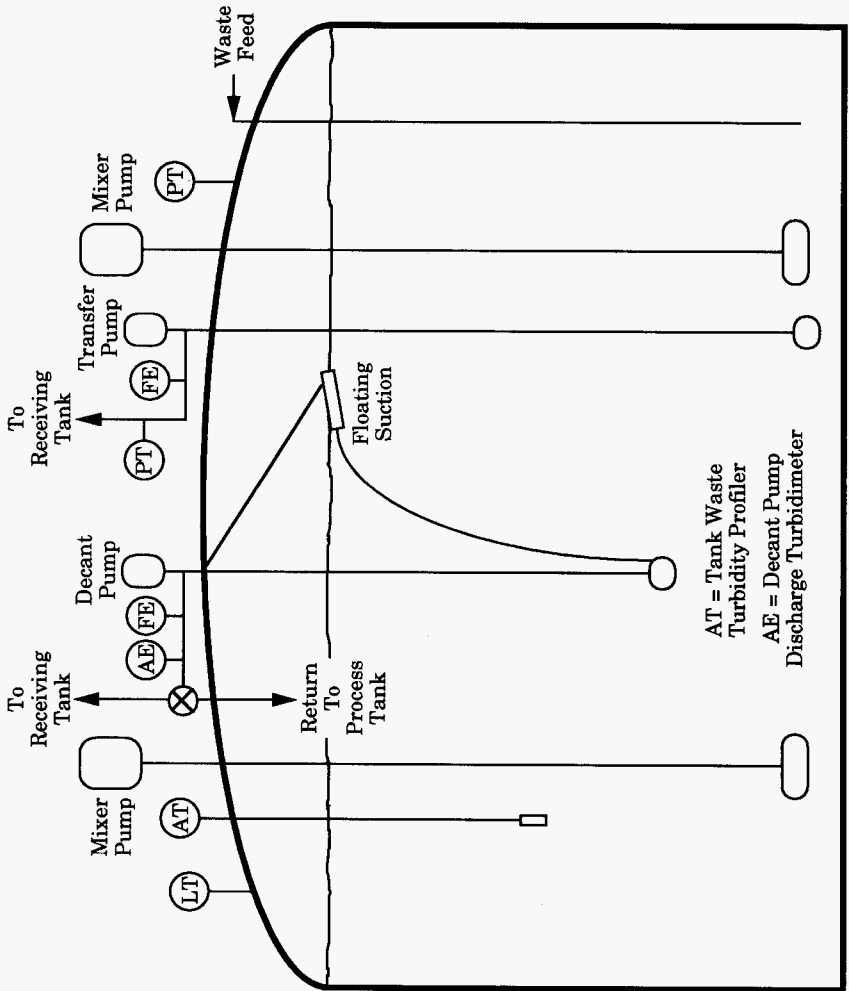
¹⁴Supernates that clear in less than a month may be decanted any time a receiver tank is available.

Figure 15
In-Tank Enhanced Sludge
Washing Diagram



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Fig. 16 Typical DST Equipment & Instruments



GTM
 6/14/95

3.2.2 Caustic Leach

After a 1.3 million-liter batch of solids is accumulated in a first-stage settling tank, sodium hydroxide solution is added to the tank to remobilize the solids and initiate the caustic leach process. The volume of solution added is calculated to yield a mobilized slurry that is 8 wt% solids and 3M NaOH after the leaching step has gone to completion. The remobilization of settled solids during leaching also blends the contents of the first-stage settling tank. The leaching and blending is allowed to proceed for up to 30 days if necessary. Once again, mixer pumps provide the required energy for the leaching and blending operation.

When leaching and blending is complete, the slurry in a first-stage settling tank is transferred to the first-wash tank. Thirty days is allowed for settling. The supernatant is decanted to the wash solution accumulation tank by a floating suction pump. Because the operation of the first-stage settling tanks is staggered (each requiring several months to accumulate solids), the enhanced washing process requires only one first-wash tank and the associated wash solution accumulation tank.

The flowsheet calculations do not reflect a second caustic leach at this time. As more information about the leaching process becomes available, it may be advisable to add a second leach cycle, or permanganate oxidative leach for specific wastes. This second cycle of leaching can be added with little impact to the flowsheet.

3.2.2.1 Single-Shell Tank Caustic Leach Factors

Revision 1 of the TWRs Process Flowsheet (Orme 1995) accounted for the removal of the four components of aluminum, chromium, sodium, and phosphorus during caustic leaching. Colton's (1996) updated pretreatment chemistry evaluation provides additional caustic leach factors that have been applied in the S/L SEPARATION process block. Table 14 shows the components and revised mass-weighted leach factors used in the PPTB. The caustic leach factor is the *fraction of the water-insoluble component removed by caustic leaching*. Enhanced sludge-washing results for a total of 22 SSTs are incorporated into the leach factor projection.

3.2.2.2 Double-Shell Tank Caustic Leach Factors

Caustic leach data for DSTs is currently limited to SY-103, although data for AZ-101 and AZ-102 should be available in the near future. After water washing, 88% of the aluminum was removed by caustic. After water washing, 8% of the chromium was removed by caustic. No data was available for phosphorus removal. In the absence of caustic leaching data, previous revisions of the TWRs Process Flowsheet assumed DST caustic leach factors of 0.85, 0.75, and 0.70 for aluminum, chromium, and phosphorus, respectively. Assuming that SY-103 results can be extrapolated to other DSTs, it appears that 0.85 is still reasonable for aluminum, while 0.10 is more reasonable for chromium. There is no basis for changing the phosphorus leach factor.

Table 14 Old and New SST Caustic Leach Factors

Component	Old SST Leach Factors TWRS Process Flowsheet Revision 1	New SST Leach Factors PPTB Revision 0
Al	0.67	0.60
Bi		0.003
Ca		0.02
Cr	0.60	0.10 ¹⁵
Fe		0.002
Na	0.25	0.45
P	0.74	0.70
Si		0.13
Sr		
U		0.002

3.2.2.3 Potential Chromium Problem

Estimated chromium inventory has increased as a result of efforts to establish best-basis estimates (Kupfer et al. 1996). At the same time, enhanced sludge-washing results indicate an apparent reduction in overall chromium leach efficiency (Colton 1996). While these trends are disturbing, it is premature to conclude from the available data that a serious chromium issue exists. Chromium solubility limits for glass are highly dependent on glass formulation, not to mention that operability of a top-outlet melter is currently the primary driver for preventing solid phase formation (Lambert and Kim 1994). Gaining acceptance of a two phase product, so long as it meets performance requirements, is a non-process alternative that could be explored.

¹⁵Waste of the TBP/EB type are the 2nd largest group considered in Colton's evaluation. New ESW results for BY-104 and BY-110, which represent 16 vol% of that group, show that 70% and 47% of the Cr was water soluble, respectively. Further Cr removal by caustic leaching was ineffective. Because of its large volume, this waste group accounts for a significant mass of residual Cr.

In the largest waste group, primarily REDOX evaporator bottoms, Cr was 70% water soluble, and since no caustic leach data were available, the balance of the Cr was assigned to residual solids.

These two "new" sources account for nearly 70% of the residual solid Cr in Colton's evaluation, and the significant reduction in caustic leach factor.

Several countermeasures for dealing with higher chromium concentration in glass could be considered:

Augment the standard caustic leaching process. Laboratory tests have verified that permanganate oxidative leaching can remove up to 90% of the chromium from selected sludges (Rapko et al. 1996).

Enhance chromium solubility by glass reformulation.

Enhance chromium solubility with higher melter temperature.

Leave the selection of melters to the Phase 2 HLW contractor(s). There are melters that are less sensitive to solids formation than the current top-outlet design.

It may be necessary, in future revisions of the PPTB, to implement such countermeasures if the chromium trends noted above become problematical. For the time being, the effect of chromium on glass volume is simply being documented, rather than changing the processing assumptions that were established for the PPTB (Washenfelder 1996b).

3.2.3 Dilute Caustic Washing

Dilute caustic is added to the first-wash tank (7 days allowed), the solids are mobilized and washed for 7 days, and the mobilized slurry is transferred to the second-wash tank (7 days allowed). Another month is allowed for settling in the second-wash tank, and the supernatant solution is decanted (7 days allowed). The wash is repeated two more times. The number of washing stages is determined by the desired concentration of the interstitial liquor and the assumed concentration of the settled solids layer, which is 20 wt% solids. The washed solids in the fourth-wash tank are remobilized with recycled condensate and transferred to washed-solids storage tanks that are available to accumulate and blend washed solids. In effect, a third stage of blending can occur in these tanks by combining batches of washed solids to optimize the overall composition.

3.2.4 Flocculents

A flocculating agent (polyelectrolyte) is added by in-line blending when the slurry transfers are made to the first-stage and second-stage settling tanks, and to the first-wash, second-wash, and third-wash tanks. The purpose is to promote settling. This is a conservative assumption for an early stage of flowsheet development. The effectiveness of flocculating agents with Hanford tank solids has not been demonstrated. If future experience shows that flocculating agents are not effective (or needed) for accelerating settling of Hanford solids, then the inter-tank slurry transfers to add flocculating agent are unnecessary and consolidating the entire enhanced sludge-wash process into a single tank could be considered.

3.2.5 Continuous Organic Decanting

An organic phase is present in C-103, and more is expected to be found as other SSTs are retrieved. The PPTB has included continuous organic decanting of waste liquors, leach liquors, and wash liquors to protect the downstream process from organic fouling. Currently, the contamination level of the C-103 organic phase is known, but other tanks need to be sampled and analyzed when organics are found. For the time being, the organic phase is assumed to be compatible with shipping to an incinerator. Future revisions of the PPTB may require washing with waste-compatible extractants to remove radionuclides from the organic.

3.3 CESIUM ION EXCHANGE FEED EVAPORATION¹⁶

The combined supernatants (Stream 9)¹⁷ of the enhanced sludge-washing operation are evaporated and filtered in the CsIX FEED EVAPORATION process block before ion exchange. For sizing the evaporator load, a bottoms concentration of 7M sodium is assumed. In actual practice, the chemistry of the waste supernatants will control the extent of evaporation to a point short of precipitating of salts. The evaporation is done early in the process to concentrate the waste prior to cesium ion exchange and to decrease the load on the LLW melter and offgas system. The evaporator also reduces volume in the event that the bottoms are returned to in-process storage. Evaporator bottoms returned to in-process storage may require chemical adjustment to ensure tank farm specifications for OH⁻ and NO₂⁻ are satisfied.

3.4 RADIONUCLIDE SEPARATIONS

3.4.1 Cesium Ion Exchange

All feeds to ion exchange will be processed through a deep-bed filter of glass frit or similar material, to remove solids that could adversely affect ion exchange column operations. Under normal conditions, the evaporator bottoms proceed to clarification through a glass frit deep-bed filter. Evaporated supernatants are likely to contain small amounts of solids that were entrained during decanting, that precipitated during evaporation or storage, or that were entrained during pipeline transfers to and from in-process storage.

Spent filter material is periodically flushed out and replaced with fresh frit. The spent filter bed is added to the cesium-depleted ion exchange effluent in the LLW evaporator feed tank.

¹⁶The Phase 2 private contractor could elect to forego evaporation if that is conducive to their process. However, since the evaporator in question is assumed to replace the 242-A Evaporator, TWRS would have to evaluate how to provide evaporation for tank farm volume control.

¹⁷It is assumed that facility wastes that are currently evaporated in the 242-A Evaporator will be added to the feed for the pretreatment process (i.e., facility wastes are included in the filtrates).

The CsIX process block houses a three-cycle operation in which an organic ion exchange resin is loaded with cesium, eluted with nitric acid, and regenerated with caustic. The ion exchange cycle is summarized in Table 15. The eluate, containing approximately 98% of the cesium, is concentrated to reduce its acid content and volume. Approximately 89% of the volume and 70% of the acid in the eluate is recycled for use in subsequent elutions. The cesium-depleted effluent, flushes, and regeneration streams feed forward to the LAW treatment process to be mixed with other miscellaneous LAW recycle streams.

Table 15 Cesium Ion Exchange Summary

Stream Name	Bed Volumes	Composition
Column loading	Variable (~35)	--
Feed flush	2	water
Cesium elution	6	0.5M HNO ₃
Eluate flush	0.5 1.5	water
Regeneration#1	1	0.5M NaOH
Regeneration#2	1	2.0M NaOH

3.4.1.1 Loading Cycle

During the loading cycle, two ion exchange beds in series receive filtered evaporator bottoms (Stream 14) until the cumulative breakthrough of ¹³⁷Cs approaches 1 Ci per 115 kg of treated sodium (1 Ci per 5,000 mol of sodium). The loading cycle is modeled with a resin having the properties of CS-100¹⁸, which allows a feed rate of 1 bed volume (BV)/h. Under these conditions, the second bed in series is partially loaded when the first bed is fully loaded with cesium. The typical length of a loading cycle is 24 h or greater.

¹⁸CS-100 is a trademark of Rohm and Haas. The resin has been extensively tested over several years at the Westinghouse Process Chemistry Laboratory, Pacific Northwest National Laboratory, and Los Alamos National Laboratory, but is no longer commercially available. The Phase 2 private contractor will select its own separating agent for cesium.

3.4.1.2 Elution/Regeneration Cycle

While the first pair of beds is loading, a second pair of beds is in the elution/regeneration cycle. A water flush at 2 BV/h displaces waste that remains in the two beds.¹⁹ The flush effluents are sent to LAW. A 0.5M HNO₃ cesium eluate at 1 BV/h then displaces cesium, sodium, and potassium from the resin. An eluate water flush at 2 BV/h removes any remaining eluate. The initial 25% of the flush stream goes with the eluate and the remainder with LAW. Finally, a 0.5M NaOH stream at 2 BV/h regenerates approximately 25% of the resin back to the sodium form, followed by a 2.0M NaOH stream that converts the balance of the resin to the sodium form. The spent regeneration streams go with the LAW.²⁰ The typical length of the elution/regeneration cycle is 10 to 12 h.

3.4.1.3 Eluate Concentration and Acid Recycle

The cesium eluate is concentrated to a bottoms concentration of 8M nitrate. The acidic condensate from the eluate concentrator is suitable for use as eluant in subsequent elutions. The Phase 2 contractor may elect to provide storage for the acidic cesium concentrate, but for the PPTB the concentrate is neutralized with NaOH and adjusted to DST concentration specifications (Stream 17). The additional sodium does not affect glass volume because the glass is currently chromium-limited (See Section 3.2.2.3).

3.4.1.4 Resin Degeneration

The degeneration of resin performance is reflected in the mass balance calculations. The resin is expected to lose 20% of its capacity over ten cycles.

After ten cycles, eluted and spent resin is flushed out to the LAW stream and replaced with fresh resin. The spent resin is oxidized in the LAW melter.

3.4.2 Other Radionuclide Separations

The absence of TRU/Sr and Tc removal from the Phase 2 flowsheet should not be construed to mean that these separations will not be required for any portion of the Phase 2 waste. The PPTB approach to Phase 2, as conveyed in APPENDIX F, has been to model Phase 2 with the existing *TWRS Process Flowsheet* model because (1) it still provides a reasonable projection of product volume even if special separations for particular wastes are not included, (2) there was no guidance for Phase 2 other than it entails treatment of the balance of

¹⁹Practical experience with operation of this system may dictate a dilute caustic flush before the water flush, to preclude aluminum precipitation in the column, or even within the resin beads. There is a minimum ionic strength and hydroxide concentration required, which was discussed in some detail in Section 2.1.

²⁰In the future, reuse of the spent regeneration caustic in sludge washing will be considered.

the waste, and (3) selection of additional separations technology is now a private contractor responsibility.

Phase 2 is also based on a composite feed stream. Cs removal is the only separation that would be widely applied during Phase 2. TRU/Sr and Tc separation would undoubtedly be required for only a small subset of the Phase 2 feed. These special treatments will not be shown until there is a differentiation of Phase 2 feed into volumes that require special treatment (as there is in Phase 1), nor until private contractors have proposed technology to make the separations.

3.5 LOW-ACTIVITY WASTE FEED EVAPORATION

The effluent from ion exchange (Stream 18) is combined with miscellaneous streams from offgas treatment (Stream 30), filter wash liquids, recycled glass product, and other dilute process recycle streams (Stream 26), before evaporation to a 10M sodium slurry (Stream 23) in the LAW FEED EVAPORATION process block.

3.6 LOW-ACTIVITY WASTE VITRIFICATION

3.6.1 Low-Activity Waste Vitrification

The LAW VITRIFICATION process block treats LAW slurry (Stream 23) in a melter of unspecified design. The glass formulation constraints are listed in Table 16.

Table 16 LLW Glass Formulation Constraints (Orme 1996)

Al_2O_3	= 12 wt%
B_2O_3	= 5 wt%
CaO	= 4 wt%
Na ₂ O	= 20 wt%
SiO ₂	>= 50 wt%

The dry glass formers (contained in Stream 24) are tailored to the waste feed to obtain the desired glass formulation.

Glass that does not meet acceptance requirements for disposal is routed to a roll crusher for size reduction. Crushed out-of-specification rework is slurred back to evaporation and recycled to the melter for remelting. For a flowsheet assumption, approximately 1% is reworked.

The Phase 2 private contractor's plan will address strategy for compliance. The private contractor may elect to qualify the treatment process rather than providing for rework of off-specification material. In general, a qualified process would require a long period of feed validation, while a process with recycle would have less stringent feed characterization requirements as long as the product could be sampled, analyzed, and reworked if found to be out of specification.

3.6.2 Immobilized Low-Activity Waste Packaging

The ILAW package for the TWRS Process Flowsheet was a 32-m³ rectangular container intended specifically for the sulfur polymer concrete waste form. The maximum size of a rectangular container for a glass monolith has not been analyzed. Since no specific guidance is provided for Phase 2 ILAW packaging, the Phase 1 standard package is used. This is the 2.6-m³ package filled to a net volume of 2.08 m³ (80 vol%). Phase 2 produces ~85,000 ILAW packages.

3.7 LOW-ACTIVITY WASTE OFFGAS TREATMENT

The OFFGAS TREATMENT process block consists of a quench tower, venturi scrubber/separator, demister, CuO SO₂ absorber, NO_x catalytic reactor, and high-efficiency particulate air (HEPA) filtration. The quench tower, venturi scrubber, and demister are included to remove particulates entrained in the offgas. These devices also cool the offgas, condense water vapor, and condense and scrub semi-volatile waste components like technetium. There are currently no provisions to recover technetium from the decanted wastes, so the scrub will become enriched with technetium over time. Recirculated nitric acid is used as the scrub medium, so it is not effective for removal of the NO_x and SO₂, both of which are criteria air pollutants.

Sulfur dioxide is removed from the gas stream by the Shell Flue Gas Desulfurization process. Nitrogen oxides are removed by selective catalytic reduction with NH₃. A combination of washable-metal HEPA filters and paper HEPA filters are used to filter the offgas before discharge to a stack. Liquid condensates from the offgas system are routed to the LAW evaporator.

3.7.1 Sulfur Recovery

SO₂ is removed from melter offgas by trapping on a CuO bed (as CuSO₄) at 400 °C. The CuO beds are approximately 90% effective at removing SO₂. After loading, the CuSO₄ is reduced with H₂, which releases the sulfur as H₂S. The CuO bed is regenerated by purging with air.

The H₂S released from the CuO bed is burned to a stoichiometric mixture (2 H₂S to 1 SO₂) in a combustion chamber. The stoichiometric mixture is reduced to elemental sulphur in a two-stage Claus reactor. The overall conversion efficiency of the Claus reactors is 99%. The tail gas from the Claus reactor is recycled to the inlet of the CuO bed.

The recovered sulfur is poured into 55-gal drums while still molten, allowed to cool, and packed out as a secondary waste (Stream 32).

3.7.2 Chloride and Fluoride Control

The quench tower and venturi are effective at scrubbing volatile chlorine and fluorine from the melter offgas, so the scrub solution becomes enriched in chloride and fluoride. Offgas treatment includes an operation to recover and discharge chloride as a secondary solid-waste grout. Fluoride is returned to the melter in a non-volatile CaF₂ form.

The chloride recovery operation consists of diverting a side stream of the recirculating scrub solution to a series of evaporators and distillation columns. A nitric acid product stream (containing all of the entrained

solids, most of the nitric acid, 90% of the fluorine, and 35% of the chlorine) is neutralized with 10% excess $\text{Ca}(\text{OH})_2$, to precipitate CaF_2 before recycling to the LLW evaporator in Stream 30. The CaF_2 will not re-volatilize from the melter. The calcium added in this operation reduces the amount of calcium added directly to the melter.

HCl concentrate (containing 65% of the chlorine and 10% of the fluorine) is neutralized, evaporated to reduce volume, grouted, and packed out in 55-gal drums as a secondary waste (Stream 33).

3.7.3 Mercury Recovery

The OFFGAS TREATMENT process block currently *does not contain* a separation for the mercury. Most of the mercury carried in the melter offgas (Stream 27) is recovered in the nitric acid scrub medium and recycled. Stream 34 is provided strictly as a convenience to quantify how much mercury is available for separation from the chloride side stream.

3.8 HIGH-LEVEL WASTE FEED EVAPORATION

The HLW FEED EVAPORATION process block combines offgas condensates and recycled scrub liquid (Stream 36) with pretreated solids (Stream 11), and dewateres the slurry by a combination of centrifugation and evaporation to reduce the evaporative load on the HLW melter. Process condensate (Stream 37) and condenser vent (Stream 38) result from dewatering.

The dewatered solids (Stream 39) are ready for feed adjustment.

3.9 HIGH-LEVEL WASTE VITRIFICATION

The HLW VITRIFICATION process block combines Stream 39 with recovered cesium (Stream 17) and a concentrated spent scrub solution (Stream 41), performs the feed adjustment, and vitrifies the solids.

3.9.1 Feed Adjustment

For feed adjustment, glycolic acid (included in Stream 40) is added to adjust the pH to approximately 6 and provide sufficient reductant (organic carbon). An addition of 6.4 g-mol glycolic acid per kg of waste oxides is expected to provide a sufficient excess for redox/oxidation control in the melter.

The organic acid digest is followed by the dry addition of glass-former chemicals such as silica, boric oxide and lithium oxide (included in Stream 40). The feed slurry is then concentrated by evaporation to a total oxide concentration of approximately 500 g/L and transferred to one of the melter feed tanks.

3.9.2 High-Level Waste Vitrification

The melter is assumed to be a low-temperature, joule-heated, slurry-fed ceramic melter. Scaling up of the Defense Waste Processing Facility (DWPF) joule-heated melter will be necessary to provide the required throughput rate

if that design is selected. The number and sizing of melters is a Phase 2 private contractor decision.

For the flowsheet, the adjusted feed slurry from the melter feed tank is continuously fed to a joule-heated melter where slurry water is evaporated and calcination reactions proceed in the "cold cap" over the molten glass pool. Water and other volatile feed components are driven off, while nonvolatile components oxidize and melt into the glass. The molten borosilicate glass product flows (by pressure differential) from the melter into stainless-steel canisters, where the product cools to form a monolithic glass.

The process model predicts glass composition from the glass formulation ranges stated in Table 17. These ranges are for low-temperature (1150 °C) melting.

With the current formulation ranges and HLW waste feed, the waste loading in IHLW is 37% (including sodium and silicon). The reduced caustic leach factor for chromium, discussed in Section 3.2.2.1, is responsible for chromium controlling the volume of IHLW.

3.9.3 Final Packaging

When sufficiently cooled, the filled canisters are sealed with an inner canister closure plug. A preliminary decontamination is performed by a low pressure water spray that removes loose contamination. Final decontamination is accomplished by a frit-blasting process. A final canister seal is provided by a welded closure.

A variety of canisters containing somewhat different net waste volumes are available for consideration, including the DWPF canister (0.62 m³), the West Valley Demonstration Project canister (0.8 m³), or a 4.5 m tall contractor-proposed standard canister (1.08 m³) that the Office of Civilian Radioactive Waste Management may be willing to consider (Honeyman 1996). Phase 2 produces 12,890 contractor-proposed standard canisters.

3.10 HIGH-LEVEL WASTE OFFGAS TREATMENT

Offgas from the feed adjustment evaporation step is condensed and collected. Reduced mercury contained in the condensate is accumulated in a mercury sump built into the condensate collection tank. A total of 70 kg mercury (5 L) is expected to accumulate over the life of the plant.

Melter offgases (included in Stream 43 with feed adjustment vapors) flow to a quench tower and venturi scrubber to cool and condense the offgas, and separate entrained particulates from the gas stream. The offgas then passes through a chiller, demister, and HEPA filter. Levels of sulfur in the HLW melter feed will probably not require a reactor (CuO bed) for SO₂ abatement; likewise, the amount of nitrate in HLW is small so NO_x abatement is not an issue. Melter offgas exiting the HEPA filter will be combined with building ventilation exhaust air and released to the atmosphere via the plant stack.

Table 17 HLW Glass Formulation Ranges (CVS@1150 °C)

Component	Glass	
	Lower	Upper
Single-Component Ranges ^a		
Al ₂ O ₃	0.0%	15.0%
B ₂ O ₃	5.0%	20.0%
CaO	0.0%	10.0%
Fe ₂ O ₃	2.0%	15.0%
Li ₂ O	1.0%	7.0%
MgO	0.0%	8.0%
Na ₂ O ^b	5.0%	20.0%
SiO ₂	42.0%	57.0%
ZrO ₂	0.0%	13.0%
Multi-Component Ranges ^c		
Al ₂ O ₃ +ZrO ₂	<=16.0%	
Al ₂ O ₃ +ZrO ₂ +Fe ₂ O ₃	<=24.0%	
MgO+CaO	<=10.0%	
Solubility Limits		
Cr ₂ O ₃	<=0.5%	
F	<=1.7%	
P ₂ O ₅ ^d	<=3.0%	
Rh ₂ O ₃ +Ru ₂ O ₃ +Ru ₂ O ₃	<=0.25%	
SO ₂	<=0.5%	

^aThe sum of all components not listed may range from 1% to 10%.

^bIncludes K₂O.

^cAttempts to eliminate formulations with poor processability by the application of multiple component constraints have been "only partially successful" per Hrma 1994. Multi-component constraints are ignored in the model.

^dThis limit differs from the 1% ceiling used for HWVP formulations as shown in Hrma 1994. It is an engineering judgment that TWRS composite glass can solubilize up to 3% P₂O₅.

Spent scrubber solution collected from the quench tower and venturi scrubber is evaporated in the secondary waste evaporator and recycled to the feed collection tank.²¹

Because of the potential for contamination, condenser vent gases in the HLW process are all scrubbed through the condenser vent scrubber. The condenser vent scrub solutions are combined with feed adjustment condensate and returned to the HLW FEED EVAPORATION process block.

²¹The portion of the spent scrub that was previously routed to the salt waste adjustment tank purged the melter system of halides and other volatile compounds not soluble in the glass. In Revision 1, the HLW process operates beyond the completion of pretreatment and LLW treatment, and it is assumed that routing purges out of the facility is discouraged. Further study will determine if HLW scrub solution treatment similar to the LLW scrub solution treatment is required.

3.11 WATER RECYCLE

The TWRS flowsheet recycles process condensates extensively where the use of condensates is acceptable. The WATER RECYCLE process block shows where recycled water is used. Excess process condensates from the TWRS flowsheet are routed to the Liquid Effluent Treatment Facility for conditioning before release to the environment. Condensate treatment is an Environmental Restoration function outside of the scope of the TWRS Process Flowsheet.

3.12 PHASE 2 WITH REVISED TWRS INVENTORY

There is uncertainty, not directly addressed in this flowsheet, in estimating glass properties, durability, and melter operability as a function of glass formulation. There is also uncertainty in regard to the degree of chemical separation attainable in the enhanced sludge-washing process and in the waste inventories.

Appendix E contains a special case of the Phase 2 flowsheet based on a revised TWRS inventory. Standard inventory projections for several major components were substituted for the TWRS inventory values. The glass volume projection for this special case is profoundly affected by the large increase in chromium inventory left over after enhanced sludge washing. The revised TWRS inventory produces 28,460 contractor-proposed standard canisters during Phase 2.

4.0 REFERENCES

- Bacon, R. F., 1996, *Final Neutralized Current Acid Waste Consolidation Recommendation*, External Letter 9651466, R. F. Bacon to J. E. Kinzer, May 10, 1996, Westinghouse Hanford Company, Richland, Washington.
- Certa, P. J., W. H. Grams, C. M. McConville, L. W. Shelton, and E. J. Slaathaug, 1996, *Low-Level Waste Feed Staging Plan*, WHC-SD-WM-RPT-224, Revision 1, Westinghouse Hanford Company, Richland, Washington.
- Colton, N. G., 1995, *Sludge Pretreatment Chemistry Evaluation: Enhanced Sludge Washing Separation Factors*, PNL-10512, Pacific Northwest Laboratory, Richland, Washington.
- Colton, N. G., 1996, *Status Report: Pretreatment Chemistry Evaluation - Wash and Leach Factors for the Single-Shell Tank Waste Inventory*, PNNL-11290, Pacific Northwest National Laboratory, Richland, Washington.
- DOE-RL, 1996, *TWRS Privatization Request for Proposals*, DE-RP06-96RL13308, U.S. Department of Energy Richland Operations Office, Richland, Washington.
- Honeyman, J. O., 1996, *Proposed Standard Canister for Tank Waste Remediation System High-Level Waste Disposal*, External Letter 9653251, J. O. Honeyman to W. J. Taylor, August 1, 1996, Westinghouse Hanford Company, Richland, Washington.
- Hrma, P. R. et al., 1994, *Property/Composition Relationships for Hanford High-Level Waste Glasses Melting at 1150 °C*, PNL-10359, Vol. 1, Pacific Northwest Laboratory, Richland, Washington.
- Klem 1996, *Preliminary Estimate of Process Organic Volume in Waste Tanks*, Internal Memo 73510-96-029, M. J. Klem to D. J. Washenfelder, August, 1996.
- Kupfer, M. J. et al., 1996, *Interim Report: Best-Basis Inventories of Chemicals and Radionuclides in Hanford Site Tank Waste*, WHC-SD-WM-TI-740 Revision C, Westinghouse Hanford Company, Richland, Washington.
- Lambert, S. L. and D. S. Kim, 1994, *Tank Waste Remediation System High-Level Waste Feed Processability Assessment Report*, WHC-SP-1143, Westinghouse Hanford Company, Richland, Washington.
- Lumetta, G. J. and B. M. Rapko, 1994, *Washing and Alkaline Leaching of Hanford Tank Sludges: A Status Report*, PNL-10078, Pacific Northwest Laboratory, Richland Washington.
- Lumetta, G. J., B. M. Rapko, M. J. Wagner and J. Liu, *Washing and Caustic Leaching of Hanford Tank Sludges: Results of FY 1996 Studies*, PNNL-11278, Pacific Northwest National Laboratory, Richland, Washington.
- Manuel, A. F., 1996, *Phase I High-Level Waste Pretreatment and Feed Staging Plan*, WHC-SD-WM-ES-370, Revision 0, Westinghouse Hanford Company, Richland, Washington.

WHC-SD-WM-TI-774 Rev. 0
TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

- Orme, R. M., 1994, *TWRS Process Flowsheet*, WHC-SD-WM-TI-613 Revision 0, Westinghouse Hanford Company, Richland, Washington.
- Orme, R. M., 1995, *TWRS Process Flowsheet*, WHC-SD-WM-TI-613 Revision 1, Westinghouse Hanford Company, Richland, Washington.
- Penwell, D. L., C. E. Grenard and R. S. Wittman, 1996, *Initial Retrieval Sequence and Blending Strategy*, WHC-SD-WM-RPT-229 Revision 0, Westinghouse Hanford Company, Richland, Washington.
- Rapko, B. M., G. J. Lumetta, and M. J. Wagner, 1995, *Washing and Caustic Leaching of Hanford Tank Sludges: Results of FY 1995 Studies*, PNL-10712, Pacific Northwest Laboratory, Richland, Washington.
- Raytheon 1995, *Initial Pretreatment Module Trade Studies -- In-Tank vs. Out-of-Tank Pretreatment*, E/B-SD-W236B-RPT-017 Revision 1, Raytheon/BNFL, Richland, Washington.
- Shelton, L. W., 1996, *Projected Double-Shell Tank Supernatant Composition and Inventory for Phase I Privatization*, WHC-SD-WM-TI-751 Revision 0, Westinghouse Hanford Company, Richland, Washington.
- Washenfelder, D. J., 1996, *Revised TWRS Disposal Program Assumptions for Operational Waste Volume Projection*, Internal Memo 73510-96-013 dated May 14, 1996 (and amended July 29, 1996), Westinghouse Hanford Company, Richland, Washington.
- Washenfelder, D. J., 1996b, *TWRS Process Technical Baseline Assumptions and Bases*, Internal Memo 73510-96-014 dated May 7, 1996, Westinghouse Hanford Company, Richland, Washington.
- WHC, 1996, *Tank Waste Remediation System Functions and Requirements Document*, WHC-SD-WM-FRD-020, Revision 0, March 1996, Westinghouse Hanford Company, Richland, Washington.

APPENDIX A INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS

The following table projects DST supernate as it will exist per Shelton (1996), and identifies the tanks that have been selected as Phase 1 feeds. These are "as is" values. They have not been diluted by retrieval water or adjusted for retrieval inefficiencies and heel mixing like the actual feed batches in Tables 2a and 2b.

Explanation of headings:

P-o-C or Extension refers to the proof-of-concept or extension part of Phase 1.

Envelope A, B, or C refers to the Phase 1 supernate envelopes.

PC1 Batch# and PC2 Batch# refer to the private contractor feed batch in which each waste will appear.

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Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	101AN	102AN	103AN	104AN	105AN	106AN	107AN	101AP	102AP	103AP
P-o-C or Extension		Extension	P-o-C	P-o-C	P-o-C	Extension	Both			
Envelope		C	A	A	A	C	C			
PC1 Batch#		9	5	3	1	10 and 11	7 and 8			
PC2 Batch#		9	5	3	1	10	7 and 8			
Chemical (MT)										
Ag+	1.11E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.75E-04	0.00E+00	5.69E-03	0.00E+00	0.00E+00
Al(OH)4-	2.97E+01	1.97E+02	7.33E+02	3.99E+02	7.09E+02	2.81E+02	1.48E+01	1.30E+02	1.70E+02	8.85E-02
As+5	5.46E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.49E-04	0.00E+00	5.35E-03	3.69E-04	4.95E-06
B+3	1.58E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	5.78E-02	0.00E+00	0.00E+00
Ba+2	1.05E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.24E-04	0.00E+00	9.89E-03	1.18E-03	0.00E+00
Be+2	1.97E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	6.07E-04	0.00E+00
Bi+3	1.39E-01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	7.89E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ca+2	3.84E-01	1.66E+00	3.13E-01	0.00E+00	0.00E+00	4.91E-04	1.92E+00	4.25E-01	0.00E+00	0.00E+00
Cd+2	5.97E-02	0.00E+00	5.79E-02	0.00E+00	0.00E+00	5.51E-04	0.00E+00	8.10E-03	6.11E-03	1.13E-05
Ce+3	5.23E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cr(OH)4-	2.72E+00	2.48E+00	7.08E+00	4.71E+00	6.70E+00	1.21E-02	1.37E+00	1.34E+00	5.93E+00	1.04E-03
Clu+2	5.40E-03	0.00E+00	4.34E-02	0.00E+00	0.00E+00	2.04E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Fe+3	4.09E-01	0.00E+00	2.55E-01	3.37E-02	4.79E-02	7.12E-03	5.24E+00	1.11E-01	1.58E-02	1.26E-04
Hg+2	2.46E-03	0.00E+00	5.79E-02	0.00E+00	0.00E+00	1.26E-06	0.00E+00	1.15E-05	0.00E+00	5.11E-07
K+	1.48E+00	1.47E+01	5.50E+01	2.16E+01	2.63E+01	5.87E-03	7.41E+00	8.99E+01	5.37E+00	1.55E-01
La+3	6.28E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	6.07E-02	0.00E+00	0.00E+00
Li+	5.61E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mg+2	6.26E-02	0.00E+00	1.04E-01	0.00E+00	0.00E+00	1.02E-03	0.00E+00	5.09E-02	0.00E+00	1.22E-04
Mn+4	8.11E-02	0.00E+00	1.04E-01	0.00E+00	0.00E+00	9.36E-04	1.75E+00	7.40E-03	0.00E+00	4.40E-06
MnO2	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mo+6	1.63E-02	0.00E+00	3.18E-01	0.00E+00	0.00E+00	3.62E-04	0.00E+00	7.32E-04	0.00E+00	0.00E+00
Na+	2.19E+02	1.00E+03	1.22E+03	8.34E+02	1.18E+03	1.49E+03	7.78E+02	6.01E+02	4.24E+02	5.43E-01
Ni+3	8.39E-04	1.32E+00	8.68E-02	0.00E+00	0.00E+00	0.00E+00	1.57E+00	9.21E-02	1.11E-01	0.00E+00
Pb+4	8.29E-02	0.00E+00	2.61E-01	0.00E+00	0.00E+00	2.50E-03	1.15E+00	1.54E-02	1.37E-02	0.00E+00
Rb+	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Re+7	3.44E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Rh+3	3.56E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ru+3	1.13E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Sb+5	1.37E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Se+6	5.62E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.51E-06	0.00E+00	3.90E-04	1.53E-06	0.00E+00
Si+4	1.60E+00	0.00E+00	9.84E-01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	4.62E-01	0.00E+00	0.00E+00
Sn+4	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Sn+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Te+6	3.53E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Th+4	2.22E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ti+4	1.01E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.91E-05	0.00E+00	1.72E-10	0.00E+00	0.00E+00
Tl+3	2.80E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
U (g/L)	9.92E-01	0.00E+00	1.87E-03	0.00E+00	0.00E+00	8.51E-04	7.85E-01	1.50E-01	1.46E-02	3.77E-04
V+5	3.25E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
W+6	2.52E-03	0.00E+00	7.53E-01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00

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TWS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	101AN	102AN	103AN	104AN	105AN	106AN	107AN	101AP	102AP	103AP
P-o-C or Extension		Extension	P-o-C	P-o-C	P-o-C	Extension	Both			
Envelope		C	A	A	A	C	C			
PC1 Batch#		9	5	3	1	10 and 11	7 and 8			
PC2 Batch#		9	5	3	1	10	7 and 8			
Chemical (MT)										
Zn+2	3.55E-04	0.00E+00	1.74E-01	0.00E+00	0.00E+00	9.89E-03	0.00E+00	2.87E-01	0.00E+00	4.51E-05
Zr+4	6.65E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	1.51E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00
CO3-2	3.31E+01	2.53E+02	3.24E+01	8.56E+01	9.35E+01	2.35E+02	2.62E+02	8.66E+01	1.11E+02	2.63E-01
CL-	1.27E+00	1.47E+01	3.47E+01	2.27E+01	3.65E+01	6.40E-02	1.08E+01	7.51E+00	1.21E+01	5.06E-03
F-	2.20E+00	7.86E+00	2.66E+00	0.00E+00	0.00E+00	1.18E+01	0.00E+00	1.71E+01	0.00E+00	1.32E-02
SO4-2	1.65E+01	5.42E+01	5.79E+00	1.98E+01	2.81E+01	4.57E+01	4.79E+01	1.77E+01	1.88E+01	3.58E-02
NO3-	5.49E+01	8.33E+02	5.79E+02	5.81E+02	8.30E+02	1.14E+03	8.28E+02	5.70E+02	3.25E+02	4.13E-01
NO2-	4.68E+01	3.15E+02	4.99E+02	2.67E+02	5.15E+02	4.70E+02	1.72E+02	1.66E+02	1.58E+02	1.33E-01
PO4-3	4.01E+01	1.86E+01	3.36E+00	8.43E+00	8.15E+00	2.97E+01	1.85E+00	3.58E+00	4.83E+01	1.42E-02
OH-	9.64E+01	4.04E+01	3.53E+02	2.10E+02	2.66E+02	4.02E+01	6.25E+01	1.69E+02	3.81E+01	1.73E-01
TOC	7.40E+00	9.89E+01	2.66E+01	1.39E+01	1.67E+01	2.15E+02	1.50E+02	1.92E+01	1.36E+01	1.14E-02

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TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	101AN	102AN	103AN	104AN	105AN	106AN	107AN	101AP	102AP	103AP
P-o-C or Extension		Extension	P-o-C	P-o-C	P-o-C	Extension	Both			
Envelope		C	A	A	A	C	C			
PC1 Batch#		9	5	3	1	10 and 11	7 and 8			
PC2 Batch#		9	5	3	1	10	7 and 8			
Radionuclide (Ci)										
14c	2.08E+01	6.89E+01	7.24E+00	0.00E+00	0.00E+00	1.82E-03	0.00E+00	6.76E-01	2.08E+00	4.56E-04
90Sr	1.32E+05	2.16E+05	3.05E+04	2.11E+04	9.82E+03	7.71E+00	2.32E+05	1.34E+05	4.20E+03	1.81E-01
90Y	1.32E+05	2.16E+05	3.05E+04	2.11E+04	9.82E+03	7.71E+00	2.32E+05	1.34E+05	4.20E+03	1.81E-01
99Tc	3.28E+02	1.17E+03	6.15E+02	3.96E+02	5.62E+02	3.76E-01	1.08E+03	5.03E+02	3.57E+02	1.11E-01
137Cs	1.05E+06	7.16E+05	1.80E+06	1.65E+06	1.56E+06	7.26E+02	6.64E+05	4.80E+05	6.77E+05	4.62E+02
137Ba	1.00E+06	6.80E+05	1.71E+06	1.56E+06	1.48E+06	6.89E+02	6.31E+05	4.56E+05	6.43E+05	4.39E+02
154Eu	8.38E+02	3.00E+03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.18E-02	0.00E+00	0.00E+00
235U	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
238U	3.66E-01	0.00E+00	6.30E-04	0.00E+00	0.00E+00	3.10E-08	2.64E-01	6.27E-03	4.92E-03	1.27E-04
237Np	4.93E+00	0.00E+00	7.24E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
238Pu	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
239Pu	8.54E+01	2.22E+02	6.88E+00	2.51E+01	3.57E+01	1.64E-04	9.47E+01	9.59E+00	0.00E+00	0.00E+00
240Pu	3.71E+00	5.54E+01	1.72E+00	6.28E+00	8.93E+00	4.11E-05	2.37E+01	2.35E+00	0.00E+00	0.00E+00
241Pu	1.16E+01	1.87E+02	4.63E+00	2.02E+01	2.86E+01	1.32E-04	7.81E+01	7.39E+00	0.00E+00	0.00E+00
241Am	5.44E+02	2.33E+02	8.32E+00	4.58E+00	6.49E+00	3.28E-03	2.19E+03	3.01E+01	1.74E+00	0.00E+00
Volume, (L)	3.46E+06	3.84E+06	3.62E+06	3.02E+06	4.29E+06	4.00E+06	3.68E+06	4.31E+06	4.16E+06	1.02E+05
Volume, (kgal)	9.14E+02	1.01E+03	9.56E+02	7.98E+02	1.13E+03	1.06E+03	9.73E+02	1.14E+03	1.10E+03	2.70E+01
Na Molarity	2.75E+00	1.14E+01	1.46E+01	1.20E+01	1.20E+01	1.61E+01	9.19E+00	6.06E+00	4.43E+00	2.31E-01
H2O Estimate	2.98E+06	2.08E+06	1.65E+06	1.54E+06	2.05E+06	1.91E+06	2.12E+06	2.90E+06	3.09E+06	1.00E+05

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Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	104AP	105AP	106AP	107AP	108AP	101AW	102AW	103AW	104AW	105AW
P-o-C or Extension	P-o-C		P-o-C	Extension		P-o-C				
Envelope	A		A	C		A				
PC1 Batch#	2		2	11		4				
PC2 Batch#	2		2	11 and 12		4				
Chemical (MT)										
Ag+	1.18E-13	3.16E-08	5.57E-09	3.44E-05	0.00E+00	0.00E+00		0.00E+00	1.22E-09	0.00E+00
Al(OH)4-	1.13E+02	6.25E+00	4.77E+02	2.73E+02	7.77E-02	3.87E+02		7.92E-02	2.11E+00	1.89E-03
As+5	1.18E-14	2.07E-07	5.57E-10	2.24E-04	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
B+3	3.70E-08	4.87E-06	9.73E-03	5.27E-03	0.00E+00	0.00E+00		0.00E+00	7.25E-07	0.00E+00
Ba+2	7.93E-13	6.60E-06	1.27E-04	7.16E-03	1.62E-05	0.00E+00		3.03E-04	6.33E-06	9.52E-08
Be+2	7.13E-14	0.00E+00	4.42E-05	0.00E+00	6.72E-08	0.00E+00		0.00E+00	0.00E+00	3.31E-08
Bi+3	3.53E-12	0.00E+00	1.67E-07	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Ca+2	9.71E-09	2.49E-04	4.67E-02	2.71E-01	6.73E-05	1.30E-01		3.34E-03	6.08E-05	3.31E-05
Cd+2	2.35E-13	4.03E-07	1.11E-08	4.36E-04	5.89E-04	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Ce+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Cr(OH)4-	7.43E-08	1.79E-04	1.32E-01	1.96E-01	1.26E-03	1.46E+00		9.09E-02	3.56E-05	8.45E-05
Cu+2	2.35E-13	0.00E+00	1.11E-08	0.00E+00	0.00E+00	0.00E+00		0.00E+00	1.59E-07	0.00E+00
Fe+3	1.09E-02	1.27E-05	2.06E-02	1.37E-02	7.11E-04	0.00E+00		0.00E+00	6.91E-04	4.96E-03
Hg+2	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
K+	8.08E-06	7.42E-03	1.59E+01	8.33E+00	1.02E-01	1.65E+02		1.10E+01	2.45E-04	1.03E-02
La+3	0.00E+00	6.88E-05	0.00E+00	7.44E-02	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Li+	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Mg+2	8.91E-11	1.70E-05	5.40E-02	1.85E-02	8.22E-05	2.06E-01		3.71E-04	2.00E-06	4.05E-05
Mn+4	1.52E-01	0.00E+00	2.87E-02	2.55E-07	0.00E+00	1.03E-01		0.00E+00	1.31E-07	0.00E+00
MnO2	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Mo+6	4.43E-11	0.00E+00	2.38E-02	4.03E-05	3.62E-05	2.27E-01		1.40E-03	2.24E-06	1.79E-05
Na+	2.36E+02	3.30E+01	1.00E+03	1.46E+03	5.90E-01	9.06E+02		1.06E+01	1.03E+01	2.18E-01
Ni+3	2.35E-13	7.26E-05	1.11E-08	7.85E-02	4.06E-05	0.00E+00		1.60E-03	2.76E-07	0.00E+00
Pb+4	4.70E-12	1.23E-06	2.22E-07	1.37E-03	0.00E+00	1.19E+00		0.00E+00	1.41E-06	0.00E+00
Rb+	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Re+7	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Rh+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Ru+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Sb+5	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Se+6	0.00E+00	3.21E-08	0.00E+00	3.47E-05	0.00E+00	1.30E-04		0.00E+00	0.00E+00	0.00E+00
Si+4	4.42E-07	3.30E-05	1.16E-01	3.95E-02	0.00E+00	0.00E+00		1.34E-01	5.81E-07	0.00E+00
Sn+4	5.88E-12	0.00E+00	2.78E-07	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Sm+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Te+6	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Th+4	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
Ti+4	1.18E-13	1.45E-14	5.57E-09	1.57E-11	0.00E+00	1.86E-02		0.00E+00	0.00E+00	0.00E+00
Tl+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
U (g/l)	8.70E-03	3.17E-05	2.59E-02	3.44E-02	3.91E-04	8.83E-01		5.34E-03	4.93E-02	1.99E-03
V+5	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	0.00E+00	0.00E+00
W+6	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00		0.00E+00	4.55E-06	0.00E+00

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TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	104AP	105AP	106AP	107AP	108AP	101AW	102AW	103AW	104AW	105AW
P-o-C or Extension	P-o-C		P-o-C	Extension		P-o-C				
Envelope	A		A	C		A				
PC1 Batch#	2		2	11		4				
PC2 Batch#	2		2	11 and 12		4				
Chemical (MT)										
Zr+2	0.00E+00	2.55E-05	0.00E+00	2.77E-02	2.92E-08	1.25E+00		2.49E-03	5.13E-07	0.00E+00
Zr+4	5.88E-12	0.00E+00	2.78E-07	0.00E+00	0.00E+00	1.99E-01		0.00E+00	2.35E-08	0.00E+00
CO3-2	3.14E+01	5.25E+00	1.33E+02	2.39E+02	2.61E-01	4.85E+01		2.49E+00	1.10E+00	2.14E-03
CL-	1.22E+01	1.04E-03	5.02E+01	1.13E+00	5.89E-03	2.04E+01		7.31E-02	4.22E-01	4.10E-03
F-	8.37E+00	2.50E-01	4.85E+01	1.15E+01	3.64E-02	0.00E+00		9.42E+00	1.54E-02	9.45E-03
SO4-2	6.58E+00	1.02E+00	2.72E+01	4.92E+01	1.51E-02	4.06E+00		3.05E-02	5.75E-02	2.34E-02
NO3-	1.79E+02	2.53E+01	7.82E+02	1.13E+03	4.35E-01	8.43E+02		1.90E+00	8.81E+00	1.97E+00
NO2-	8.80E+01	1.05E+01	3.72E+02	4.53E+02	1.17E-01	4.02E+02		6.60E-01	1.16E+00	6.46E-02
PO4-3	6.39E+00	6.59E-01	1.97E+01	2.82E+01	2.13E-02	8.31E+00		3.14E-02	5.62E-01	2.29E-02
OH-	6.04E+01	8.94E-01	2.42E+02	5.81E+01	1.58E-01	3.40E+02		1.73E+00	3.83E+00	7.51E-02
TOC	6.34E+00	4.78E+00	2.23E+01	2.03E+02	5.07E-02	9.69E+00		5.06E-01	9.16E-01	2.39E-02

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Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	104AP	105AP	106AP	107AP	108AP	101AW	102AW	103AW	104AW	105AW
P-o-C or Extension	P-o-C		P-o-C	Extension		P-o-C				
Envelope	A		A	C		A				
PC1 Batch#	2		2	11		4				
PC2 Batch#	2		2	11 and 12		4				
Radionuclide (Ci)										
14C	1.38E-12	4.95E-05	1.89E-07	5.35E-02	7.72E-10	1.45E+00	0.00E+00	0.00E+00	1.39E-05	0.00E+00
90Sr	1.72E-05	1.50E+02	1.18E-01	1.64E+05	5.41E-03	2.81E+03	0.00E+00	8.55E-02	6.85E-03	0.00E+00
90Y	1.72E-05	1.50E+02	1.18E-01	1.64E+05	5.41E-03	2.81E+03	0.00E+00	8.55E-02	6.85E-03	0.00E+00
99Tc	3.14E-07	3.50E-01	1.49E-02	3.78E+02	2.05E-02	5.94E+02	0.00E+00	1.23E+01	5.26E-03	1.01E-02
137Cs	1.42E-02	1.39E+02	2.81E+02	1.52E+05	1.70E+02	1.29E+06	0.00E+00	8.14E+03	7.72E+00	7.86E+01
137Ba	1.35E-02	1.32E+02	2.67E+02	1.44E+05	1.61E+02	1.22E+06	0.00E+00	7.74E+03	7.33E+00	7.46E+01
154Eu	0.00E+00	0.00E+00	0.00E+00	3.84E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
235U	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
238U	4.18E-12	7.12E-06	2.00E-07	7.69E-03	4.29E-06	2.97E-01	0.00E+00	1.79E-03	6.04E-07	1.90E-06
237Np	5.61E-07	0.00E+00	9.78E-03	0.00E+00	4.16E-08	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
238Pu	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
239Pu	3.23E-06	1.04E-02	1.44E-02	1.13E+01	0.00E+00	3.63E+00	0.00E+00	0.00E+00	4.47E-05	0.00E+00
240Pu	2.06E-07	2.61E-03	3.59E-03	2.82E+00	0.00E+00	9.07E-01	0.00E+00	0.00E+00	8.81E-07	0.00E+00
241Pu	5.12E-07	8.13E-03	1.12E-02	8.95E+00	0.00E+00	2.49E+00	0.00E+00	0.00E+00	2.96E-06	0.00E+00
241Am	4.78E-05	3.27E-02	4.15E-04	3.53E+01	9.50E-12	4.73E+00	0.00E+00	0.00E+00	3.25E-04	0.00E+00
Volume, (L)	4.22E+06	9.99E+04	4.10E+06	4.10E+06	1.02E+05	3.94E+06	0.00E+00	5.41E+05	2.27E+06	1.00E+05
Volume, (kgal)	1.11E+03	2.64E+01	1.08E+03	1.08E+03	2.68E+01	1.04E+03	0.00E+00	1.43E+02	6.00E+02	2.64E+01
Na Molarity	2.43E+00	1.44E+01	1.06E+01	1.55E+01	2.53E-01	1.00E+01		8.52E-01	1.97E-01	9.47E-02
H2O Estimate	3.56E+06	5.09E+04	2.09E+06	1.98E+06	9.97E+04	1.92E+06		5.04E+05	2.24E+06	9.75E+04

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Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	106AW	101AY	102AY	101AZ	102AZ	101SY	101SY-TOT	102SY	103SY	103SY-TOT
P-o-C or Extension		Both								
Envelope		B								
PC1 Batch#		6 and 12								
PC2 Batch#		6								
Chemical (MT)										
Ag+	0.00E+00	2.14E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Al(OH)4-	1.04E+02	1.84E-02	4.86E+00	6.47E-02	1.02E+01	6.52E+02	8.49E-01	4.99E+01	4.92E+02	
As+5	0.00E+00	0.00E+00	9.02E-04	4.40E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
B+3	0.00E+00	2.47E-05	3.06E-04	2.43E-04	0.00E+00	0.00E+00	2.06E-11	1.55E-02	1.14E-01	
Ba+2	2.09E-04	1.97E-05	3.24E-05	3.40E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	2.93E-02	
Be+2	0.00E+00	0.00E+00	3.67E-07	2.25E-06	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Bi+3	0.00E+00	2.68E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ca+2	7.57E-03	7.20E-04	5.44E-04	1.18E-03	5.11E-02	3.68E+00	5.35E-12	2.06E-02	8.45E-01	
Cd+2	0.00E+00	1.15E-04	2.00E-05	3.83E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ce+3	0.00E+00	0.00E+00	8.23E-04	4.31E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Cr(OH)4-	1.03E+01	9.94E-04	2.87E-01	1.93E-01	1.28E-02	2.72E+00	4.11E-11	1.32E-02	4.81E+01	
Cu+2	0.00E+00	9.63E-06	7.07E-05	3.11E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Fe+3	3.63E-04	7.85E-04	1.65E-04	3.23E-04	1.34E-03	1.43E-01	3.62E-04	0.00E+00	5.52E+00	
Hg+2	0.00E+00	4.75E-06	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
K+	1.26E+01	0.00E+00	5.71E-01	2.77E-02	3.37E-01	1.90E+01	4.48E-09	6.81E-01	1.27E+01	
La+3	2.23E-03	1.20E-04	6.21E-05	6.92E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Li+	0.00E+00	0.00E+00	1.53E-04	3.13E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mg+2	4.85E-04	1.20E-04	2.95E-05	3.90E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mn+4	0.00E+00	1.56E-04	1.51E-05	2.93E-05	0.00E+00	0.00E+00	5.88E-03	0.00E+00	0.00E+00	0.00E+00
MnO2	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Mo+6	0.00E+00	0.00E+00	4.65E-03	7.15E-04	1.01E-02	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Na+	4.36E+02	8.39E+00	1.43E+01	7.63E+00	1.83E+01	1.19E+03	2.00E+00	1.66E+02	7.12E+02	
Ni+3	2.28E-03	0.00E+00	4.32E-05	7.44E-05	3.54E-03	1.70E-01	0.00E+00	8.45E-03	2.76E-01	
Pb+4	0.00E+00	1.55E-04	3.25E-04	1.53E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Rb+	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Re+7	0.00E+00	0.00E+00	7.66E-05	2.32E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Rh+3	0.00E+00	0.00E+00	5.47E-04	2.97E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ru+3	0.00E+00	0.00E+00	2.61E-04	7.36E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Sb+5	0.00E+00	0.00E+00	7.07E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Se+6	0.00E+00	0.00E+00	1.33E-03	3.61E-04	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Si+4	1.37E+00	2.32E-03	1.92E-02	4.28E-02	0.00E+00	0.00E+00	2.46E-10	1.38E-02	0.00E+00	
Sn+4	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Sm+3	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Te+6	0.00E+00	0.00E+00	1.42E-03	9.20E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Th+4	0.00E+00	0.00E+00	1.15E-03	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Ti+4	0.00E+00	0.00E+00	4.07E-04	2.59E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
Tl+3	0.00E+00	0.00E+00	1.42E-02	6.34E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
U (g/L)	3.96E+00	3.63E-05	2.79E-03	1.15E-01	2.31E-04	0.00E+00	2.90E-04	4.91E-04	1.59E+00	
V+5	0.00E+00	0.00E+00	4.90E-05	2.73E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
W+6	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00

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Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	106AW	101AY	102AY	101AZ	102AZ	101SY	101SY-TOT	102SY	103SY	103SY-TOT
P-o-C or Extension		Both								
Envelope		B								
PC1 Batch#		6 and 12								
PC2 Batch#		6								
Chemical (MT)										
Zn+2		3.94E-04	0.00E+00	7.28E-05	1.47E-05	7.15E-03	0.00E+00	0.00E+00	0.00E+00	4.86E-02
Zr+4		0.00E+00	0.00E+00	2.50E-05	7.15E-05	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
CO3-2		1.65E+02	1.80E-02	2.66E+00	1.89E+00	0.00E+00	0.00E+00	2.61E-01	2.06E+01	9.37E+01
CL-		5.57E-01	5.72E-04	1.46E-02	0.00E+00	9.40E-01	4.82E+01	1.02E-01	2.02E+00	3.12E+01
F-		7.52E+00	8.59E-04	2.67E-01	7.59E-02	0.00E+00	6.95E-01	6.03E-02	9.81E-01	3.32E+00
SO4-2		9.26E+01	7.48E-03	1.30E+00	1.13E+00	9.33E-02	2.54E+01	6.17E-02	3.97E+00	1.68E+01
NO3-		2.69E+02	2.13E-02	7.37E+00	1.60E+00	1.55E+01	2.65E+02	1.36E+00	1.30E+02	4.91E+01
NO2-		2.48E+02	1.47E+00	6.52E+00	2.73E+00	1.34E+01	2.28E+02	6.70E-01	6.59E+01	3.73E+02
PO4-3		4.13E+00	7.63E-02	1.23E-01	3.50E-03	5.40E-01	4.01E+01	1.05E-01	3.13E+00	4.01E+01
OH-		4.06E+01	2.75E+01	1.87E+00	2.05E+00	2.81E+00	7.26E+02	6.13E-01	8.40E+00	7.41E+01
TOC		7.42E+00	1.14E-02	8.63E-02	1.11E-01	9.33E-01	9.44E+01	9.30E-02	2.05E+01	7.04E+00

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Table A-1 INVENTORY ESTIMATES OF DST SUPERNATES & PHASE 1 FEEDS (ENVELOPES A, B, AND C) (10 sheets)

Supernatant	101AY	102AY	101AZ	102AZ	101SY	101SY-TOT	102SY	103SY	103SY-TOT
P-o-C or Extension	Both								
Envelope	B								
PC1 Batch#	6 and 12								
PC2 Batch#	6								
Radionuclide (G)									
14C	7.73E+00	0.00E+00	3.59E+00	1.64E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
90Sr	8.76E+03	9.46E+00	6.83E+04	8.42E+01	1.72E+02	3.08E+04	5.20E-07	2.23E+02	6.37E+04
90Y	8.76E+03	9.46E+00	6.83E+04	8.42E+01	1.72E+02	3.08E+04	5.20E-07	2.23E+02	6.37E+04
99Tc	1.53E+03	2.40E-01	4.08E+01	1.46E+01	7.56E+00	2.57E+03	0.00E+00	1.93E+01	1.88E+03
137Cs	4.51E+06	3.28E+02	1.70E+05	7.05E+04	2.90E+04	9.75E+05	1.12E-05	2.99E+04	8.25E+05
137Ba	4.28E+06	3.12E+02	1.62E+05	6.69E+04	2.76E+04	9.26E+05	1.06E-05	2.84E+04	7.83E+05
154Eu	1.21E+04	0.00E+00	3.00E+02	3.03E+01	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
235U	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
238U	1.33E+00	0.00E+00	0.00E+00	4.33E-02	7.77E-05	0.00E+00	0.00E+00	1.65E-04	0.00E+00
237Np	3.26E-01	0.00E+00	3.09E-01	5.14E-01	0.00E+00	0.00E+00	3.11E-10	0.00E+00	0.00E+00
238Pu	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00	0.00E+00
239Pu	5.54E+01	1.37E-01	4.45E-02	1.74E+00	7.95E-03	8.81E+00	8.33E-08	5.80E-03	1.14E+01
240Pu	1.39E+01	1.80E-05	1.11E-02	4.35E-01	1.99E-03	2.39E+00	1.14E-10	1.45E-03	3.11E+00
241Pu	2.96E+01	6.11E-05	3.81E-02	1.49E+00	5.68E-03	5.85E+00	3.74E-10	3.14E-03	9.25E+00
241Am	8.44E+01	2.72E-03	2.79E+02	1.04E-01	4.97E-02	8.03E+01	1.70E-06	2.07E-01	8.21E+01
Volume, (L)	4.18E+06	2.90E+06	6.25E+05	1.16E+06	6.81E+04	7.37E+06	9.98E+04	6.43E+05	4.42E+06
Volume, (kgal)	1.11E+03	7.66E+02	1.65E+02	3.06E+02	1.80E+01	1.95E+03	2.64E+01	1.70E+02	1.17E+03
Na Molarity	4.53E+00	1.26E-01	9.96E-01	2.87E-01	1.17E+01	7.00E+00	8.72E-01	1.12E+01	7.00E+00
H2O Estimate	3.06E+06	2.86E+06	5.86E+05	1.14E+06	2.97E+04	5.00E+06	9.39E+04	3.52E+05	3.00E+06

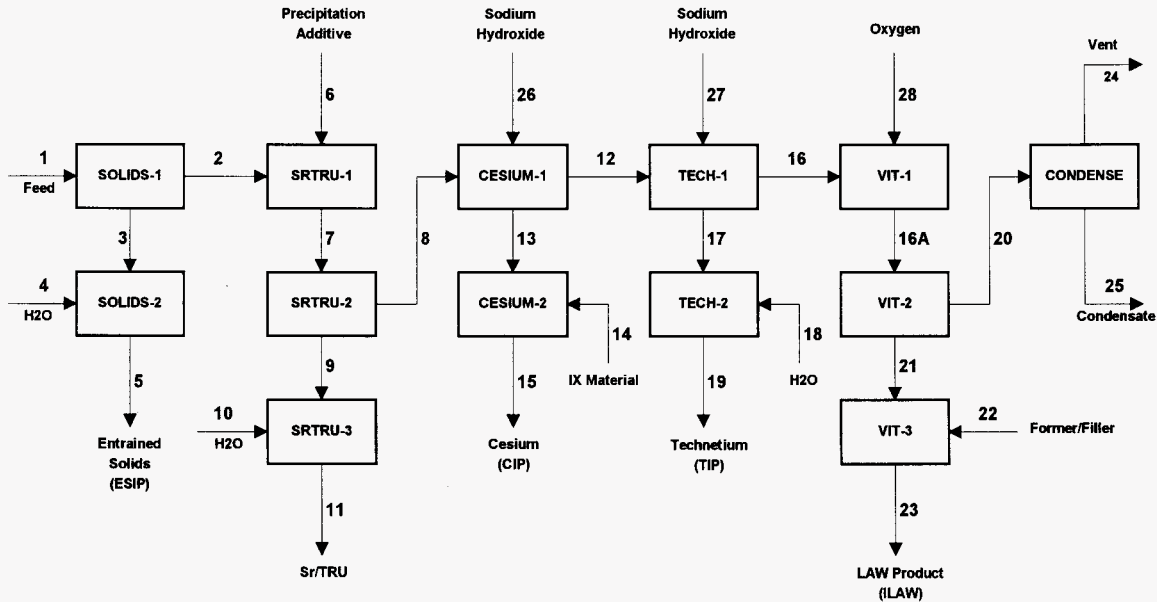
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APPENDIX B MASS BALANCES FOR ENVELOPE A, B, AND C PROCESSING

Private Contractor 1 Batches 1 to 12

Private Contractor 2 Batches 1 to 12

Figure B-1 Phase 1 Private Contractor LAW Processing



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Table B-1 Phase 1 LAW Mass Balance for Batch PCL/1 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.34E+06	3.33E+06	1.63E+04	4.05E+05	4.22E+05		3.33E+06	3.33E+06		
Density (g/L)	1.44E+03	1.44E+03	1.44E+03	1.00E+03	1.02E+03		1.44E+03	1.44E+03		
Total Mass Flow (kg)	4.82E+06	4.79E+06	2.38E+04	4.05E+05	4.29E+05		4.79E+06	4.79E+06		
RADIONUCLIDES (Ci)										
Cesium	1.03E+06	1.03E+06	5.10E+03		5.10E+03		1.03E+06	1.03E+06		
Strontium	6.62E+03	6.59E+03	3.27E+01		3.27E+01		6.59E+03	6.59E+03		
Technetium	2.71E+02	2.70E+02	1.34E+00		1.34E+00		2.70E+02	2.70E+02		
TU	2.39E+01	2.38E+01	1.18E-01		1.18E-01		2.38E+01	2.38E+01		
CHEMICALS (kg)										
AGP	8.73E-08	8.68E-08	4.31E-10		4.31E-10		8.68E-08	8.68E-08		
AL(OH)3	3.43E+05	3.41E+05	1.69E+03		1.69E+03		3.41E+05	3.41E+05		
AP+3	8.99E-04	8.94E-04	4.44E-06		4.44E-06		8.94E-04	8.94E-04		
AS+5	8.40E-03	8.36E-03	4.15E-05		4.15E-05		8.36E-03	8.36E-03		
Bv3	1.52E-01	1.51E-01	7.51E-04		7.51E-04		1.51E-01	1.51E-01		
Bv2	2.59E-02	2.57E-02	1.43E-04		1.43E-04		2.57E-02	2.57E-02		
BE+2	1.45E-02	1.44E-02	7.17E-05		7.17E-05		1.44E-02	1.44E-02		
BI+3	2.61E-06	2.60E-06	1.29E-08		1.29E-08		2.60E-06	2.60E-06		
C-14	1.06E-05	1.06E-05	5.25E-08		5.25E-08		1.06E-05	1.06E-05		
CA+2	7.30E-01	7.27E-01	3.61E-03		3.61E-03		7.27E-01	7.27E-01		
CD+2	1.39E-01	1.38E-01	6.87E-04		6.87E-04		1.38E-01	1.38E-01		
CL-	1.81E+04	1.81E+04	8.96E+01		8.96E+01		1.81E+04	1.81E+04		
CL2										
CO2										
CO3-2	4.83E+04	4.81E+04	2.39E+02		2.39E+02		4.81E+04	4.81E+04		
CR(OH)4-	2.27E+03	2.25E+03	1.61E+01		1.61E+01		2.25E+03	2.25E+03		
CSF	1.19E+01	1.18E+01	5.89E-02		5.89E-02		1.18E+01	1.18E+01		
CLH2	1.74E-07	1.73E-07	8.58E-10		8.58E-10		1.73E-07	1.73E-07		
F-	7.58E+02	7.54E+02	3.74E+00		3.74E+00		7.54E+02	7.54E+02		
F2										
FE+3	2.31E+01	2.30E+01	1.14E-01	4.05E+05	1.14E-01		2.30E+01	2.30E+01		
BD	3.00E+06	2.98E+06	1.48E+04		4.20E+05		2.98E+06	2.98E+06		
K+	1.27E+04	1.26E+04	6.27E+01		6.27E+01		1.26E+04	1.26E+04		
MG+2	8.44E-01	8.40E-01	4.17E-03		4.17E-03		8.40E-01	8.40E-01		
MH+4	4.49E-01	4.47E-01	2.22E-03		2.22E-03		4.47E-01	4.47E-01		
MD+6	3.72E-01	3.71E-01	1.84E-03		1.84E-03		3.71E-01	3.71E-01		
NH+	5.79E+05	5.76E+05	2.86E+03		2.86E+03		5.76E+05	5.76E+05		
NI+3	2.52E+00	2.51E+00	1.25E-02		1.25E-02		2.51E+00	2.51E+00		
NO2										
NO2-	2.51E+05	2.49E+05	1.24E+03		1.24E+03		2.49E+05	2.49E+05		
NO3-	4.08E+05	4.06E+05	2.01E+03		2.01E+03		4.06E+05	4.06E+05		
NP+4	2.17E-04	2.16E-04	1.07E-06		1.07E-06		2.16E-04	2.16E-04		
O2										
OH-	1.29E+05	1.28E+05	6.36E+02		6.36E+02		1.28E+05	1.28E+05		
OH+4	3.12E-01	3.10E-01	1.54E-03		1.54E-03		3.10E-01	3.10E-01		
FO+3	5.21E+03	5.18E+03	2.57E+01		2.57E+01		5.18E+03	5.18E+03		
FM+4	2.87E-01	2.85E-01	1.42E-03		1.42E-03		2.85E-01	2.85E-01		
SE+6	3.47E-05	3.46E-05	1.72E-07		1.72E-07		3.46E-05	3.46E-05		
SI+4	1.81E+00	1.81E+00	8.96E-03		8.96E-03		1.81E+00	1.81E+00		
SN+4	4.35E-06	4.32E-06	2.15E-08		2.15E-08		4.32E-06	4.32E-06		
SD+2	1.40E+04	1.39E+04	6.91E+01		6.91E+01		1.39E+04	1.39E+04		
SM+2	4.76E-02	4.74E-02	2.35E-04		2.35E-04		4.74E-02	4.74E-02		
TCD+4	2.63E+01	2.61E+01	1.30E-01		1.30E-01		2.61E+01	2.61E+01		
TI+4	8.73E-08	8.68E-08	4.31E-10		4.31E-10		8.68E-08	8.68E-08		
TCL	8.44E+03	8.40E+03	4.17E+01		4.17E+01		8.40E+03	8.40E+03		
UC2+2	1.12E+00	1.11E+00	5.51E-03		5.51E-03		1.11E+00	1.11E+00		
ZR+4	4.35E-06	4.32E-06	2.15E-08		2.15E-08		4.32E-06	4.32E-06		

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Table B-1 Phase 1 LAW Mass Balance for Batch PCL/1 (6 sheets)

STREAM NAME SOLID COMPONENTS	1	2	3	4	5	6	7	8	9	10
Total Mass Flow (kg)	4.81E+04	4.81E+02	4.76E+04		4.76E+04		4.81E+02	4.81E+02		
RADIONUCLIDES (Cl)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
BI2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
FE2O3										
FORMER										
D2WAT										
K2O										
K2O										
NaO2										
NaO2										
Na2O										
Ni2O3										
NiO2										
P2O5										
PbO2										
PuO2										
SEB3										
SiO2										
SiO2										
SO3										
SOLIDS	4.81E+04	4.81E+02	4.76E+04		4.76E+04		4.81E+02	4.81E+02		
SrO										
Ti2O7										
TiO2										
UO3										
ZrO2										

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Table B-1 Phase 1 LAW Mass Balance for Batch PCL/1 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.33E+06	3.03E+03		3.03E+03	3.33E+06	4.80E+06		1.00E-09	1.00E-09
Density (g/L)		1.44E+03	3.33E+03		3.33E+03	1.44E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.79E+06	1.01E+04		1.01E+04	4.79E+06	4.80E+06		1.00E-09	1.00E-09
RADIONUCLIDES (Ci)										
Cesium		4.42E+03	1.02E+06		1.02E+06	4.42E+03				
Strontium		6.59E+03				6.59E+03				
Technetium		2.67E+02	2.71E+00		2.71E+00	2.67E+02				
IU		2.38E+01				2.38E+01				
CHEMICALS (kg)										
AGP		8.68E-08				8.68E-08				
AL(CH ₃) ₄ -		3.41E+05				3.41E+05				
AM+3		8.94E-04				8.94E-04				
AS+5		8.36E-03				8.36E-03				
BA+2		1.51E-01				1.51E-01				
BA+2		2.87E-02				2.87E-02				
BE+2		1.44E-02				1.44E-02				
BI+3		2.60E-06				2.60E-06				
C-14		1.06E-05				1.06E-05				
CA+2		7.27E-01				7.27E-01				
CD+2		1.38E-01				1.38E-01				
CL-		1.81E+04				1.81E+04				
CL ₂							1.81E+04			
CO ₂							6.60E+04			
CO ₂ -2		4.81E+04				4.81E+04				
CR(CH ₃) ₄ -		3.25E+03				3.25E+03				
CS+		5.10E-02	1.18E+01		1.18E+01	5.10E-02				
CU+2		1.73E-07				1.73E-07				
F-		7.54E+02				7.54E+02				
F ₂							7.54E+02			
FE+3		2.30E+01				2.30E+01				
H ₂ O		2.98E+06				2.98E+06	3.18E+06		1.00E-09	1.00E-09
K+		1.26E+04				1.26E+04				
MG+2		8.40E-01				8.40E-01				
MN+4		4.47E-01				4.47E-01				
MO+6		3.71E-01				3.71E-01				
NA+		5.76E+05	5.79E+03		5.79E+03	5.76E+05				
NI+3		2.51E+00				2.51E+00				
NO ₂							5.50E+05			
NO ₂ -		2.49E+05				2.49E+05				
NO ₃ -		4.06E+05				4.06E+05				
NO ₃ +4		2.16E-04				2.16E-04				
O ₂							9.83E+05			
OH-		1.28E+05	4.28E+03		4.28E+03	1.28E+05				
PH+4		3.10E-01				3.10E-01				
PO ₄ -3		5.18E+03				5.18E+03				
RU+4		2.86E-01				2.86E-01				
SE+6		3.46E-05				3.46E-05				
SI+4		1.81E+00				1.81E+00				
SN+4		4.32E-06				4.32E-06				
SO ₄ -2		1.39E+04				1.39E+04				
SR+2		4.74E-02				4.74E-02				
TIO ₄ -		2.59E+01	2.63E-01		2.63E-01	2.59E+01				
TI+4		8.68E-08				8.68E-08				
TIC		8.40E+03				8.40E+03				
UO ₂ -2		1.11E+00				1.11E+00				
ZR+4		4.32E-06				4.32E-06				

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Table B-1 Phase 1 LAW Mass Balance for Batch PCL/1 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.81E+02		5.79E+03	5.79E+03	4.81E+02	9.93E+05			
RADIONUCLIDES (Ci)										
Cesium							4.42E+03			
Strontium							6.59E+03			
Technetium							2.67E+02			
TU							2.36E+01			
CHEMICALS (kg)										
AC2O							9.33E-08			
AL2O3							1.83E+05			
AM2O3							9.83E-04			
AS2O5							1.28E-02			
B2O3							4.87E-01			
B4O							3.21E-02			
B2O							4.01E-02			
BL2O3							2.90E-06			
CaO							1.02E+00			
ClO							1.58E-01			
CR2O3							2.06E+03			
CS2O							5.40E-02			
CUO							2.16E-07			
FE2O3							3.28E+01			
FORMER										
DMPT				5.79E+03	5.79E+03					
K2O							1.52E+04			
K2O							1.39E+00			
MO2							7.08E-01			
MO3							5.56E-01			
Na2O							7.77E+05			
NI2O3							3.54E+00			
NEO2							2.45E-04			
PO5							3.87E+03			
PO2							3.58E-01			
PUO2							3.24E-01			
SEO3							5.56E-05			
SiO2							3.86E+00			
SN2							5.49E-06			
SO3							1.16E+04			
SULFUR		4.81E+02				4.81E+02				
SFO							5.58E-02			
TC2O7							2.46E+01			
TiO2							1.45E-07			
UO3							1.16E+00			
ZRO2							5.84E-06			

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Table B-1 Phase 1 LAW Mass Balance for Batch PCL/1 (6 sheets)

SIREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.80E+06				1.62E+06	3.18E+06	3.02E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	4.80E+06				1.62E+06	3.18E+06	1.01E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Cl)									
Cesium									
Strontium									
Technetium									
IU									
CHEMICALS (kg)									
AD+									
AL(OH)4-									
AM+3									
AS+5									
Br+3									
Br+2									
Br+3									
C-14									
Ca+2									
CD+2									
Cl-									
CL2	1.81E+04				1.81E+04				
CO2	6.60E+04				6.60E+04				
CO3-2									
CR(OH)4-									
CS+									
ClH2									
F-									
F2	7.54E+02				7.54E+02				
FE+3									
H2O	3.18E+06					3.18E+06			
K+									
ME+2									
UN+4									
ND+6									
NH+							5.79E+03	5.75E-10	
NI+3									
NO2	5.50E+05				5.50E+05				
NO2-									
NO3-									
NE+4	9.85E+05				9.85E+05				1.00E+06
O2							4.28E+03	4.25E-10	
OH-									
OH+									
SO4-3									
SI+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TiO4-									
TI+4									
TiC									
UO2+2									
Zr+4									

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Table B-1 Phase 1 LAW Mass Balance for Batch PCL/1 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		9.93E+05	3.61E+06	4.60E+06					
RADIONUCLIDES (Ci)									
Cesium		4.42E+03		4.42E+03					
Strontium		6.59E+03		6.59E+03					
Technetium		2.67E+02		2.67E+02					
TRU		2.36E+01		2.36E+01					
CHEMICALS (kg)									
AC2O		9.33E-08		9.33E-08					
AL2O3		1.83E+05		1.83E+05					
AM2O3		9.83E-04		9.83E-04					
AS2O5		1.28E-02		1.28E-02					
B2O3		4.87E-01		4.87E-01					
B4O		3.21E-02		3.21E-02					
B8O		4.01E-02		4.01E-02					
BL2O3		2.90E-06		2.90E-06					
CaO		1.02E+00		1.02E+00					
ClO		1.58E-01		1.58E-01					
CR2O3		2.06E+03		2.06E+03					
CS2O		5.40E-02		5.40E-02					
CUO		2.16E-07		2.16E-07					
FE2O3		3.28E+01		3.28E+01					
FORMER			3.61E+06						
DMFAT									
FeO		1.52E+04		1.52E+04					
FeO		1.39E+00		1.39E+00					
FeO2		7.08E-01		7.08E-01					
FeO3		5.56E-01		5.56E-01					
Na2O		7.77E+05		7.77E+05					
Ni2O3		3.54E+00		3.54E+00					
NiO2		2.45E-04		2.45E-04					
FeO5		3.87E+03		3.87E+03					
FeO2		3.58E-01		3.58E-01					
HUO2		3.24E-01		3.24E-01					
SiO3		5.56E-05		5.56E-05					
SiO2		3.86E+00		3.86E+00					
SiO2		5.49E-06		5.49E-06					
SiO		1.16E+04		1.16E+04					
SULFIDS		4.81E+02		4.81E+02					
SrO		5.58E-02		5.58E-02					
Ti2O7		2.46E+01		2.46E+01					
TiO2		1.45E-07		1.45E-07					
UO3		1.18E+00		1.18E+00					
ZrO2		5.84E-06		5.84E-06					

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Table B-2 Phase 1 IAW Mass Balance for Batch PCL/2 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.82E+06	3.80E+06	1.95E+04	4.52E+05	4.72E+05		3.80E+06	3.80E+06		
Density (g/L)	1.41E+03	1.41E+03	1.41E+03	1.00E+03	1.02E+03		1.41E+03	1.41E+03		
Total Mass Flow (kg)	5.38E+06	5.35E+06	2.75E+04	4.52E+05	4.80E+05		5.35E+06	5.35E+06		
RADIONUCLIDES (Ci)										
Cesium	6.12E+04	6.09E+04	3.12E+02		3.12E+02		6.09E+04	6.09E+04		
Strontium	6.23E+03	6.23E+03	3.15E+01		3.15E+01		6.23E+03	6.23E+03		
Technetium	2.48E+01	2.47E+01	1.27E-01		1.27E-01		2.47E+01	2.47E+01		
Iru	2.57E+00	2.55E+00	1.31E-02		1.31E-02		2.55E+00	2.55E+00		
CHEMICALS (kg)										
AG+	1.61E-01	1.60E-01	8.20E-04		8.20E-04		1.60E-01	1.60E-01		
AL(OH)4-	2.92E+05	2.91E+05	1.49E+03		1.49E+03		2.91E+05	2.91E+05		
AM+3	3.12E-04	3.10E-04	1.59E-06		1.59E-06		3.10E-04	3.10E-04		
AG+5	9.33E-02	9.29E-02	4.76E-04		4.76E-04		9.29E-02	9.29E-02		
Br+	4.56E+00	4.54E+00	2.33E-02		2.33E-02		4.54E+00	4.54E+00		
BA+2	3.15E-01	3.13E-01	1.61E-03		1.61E-03		3.13E-01	3.13E-01		
BE+2	2.08E-02	2.07E-02	1.06E-04		1.06E-04		2.07E-02	2.07E-02		
BI+3	7.60E-05	7.56E-05	3.88E-07		3.88E-07		7.56E-05	7.56E-05		
C-14	1.47E-06	1.46E-06	7.50E-09		7.50E-09		1.46E-06	1.46E-06		
CA+2	2.93E+01	2.91E+01	1.50E-01		1.50E-01		2.91E+01	2.91E+01		
CD+2	1.18E-01	1.17E-01	6.00E-04		6.00E-04		1.17E-01	1.17E-01		
CL-	2.93E+04	2.91E+04	1.50E+02		1.50E+02		2.91E+04	2.91E+04		
CL2										
ClO2										
CO3-2	8.26E+04	8.22E+04	4.22E+02		4.22E+02		8.22E+04	8.22E+04		
CR(OH)4-	2.43E+02	2.43E+02	1.25E+00		1.25E+00		2.43E+02	2.43E+02		
CS+	7.07E-01	7.03E-01	3.61E-03		3.61E-03		7.03E-01	7.03E-01		
ClH2	5.06E-06	5.04E-06	2.58E-08		2.58E-08		5.04E-06	5.04E-06		
EU-154	7.94E-10	7.90E-10	4.05E-12		4.05E-12		7.90E-10	7.90E-10		
F-	2.64E+04	2.63E+04	1.35E+02		1.35E+02		2.63E+04	2.63E+04		
F2										
FE+3	1.83E+01	1.82E+01	9.35E-02	4.52E+05	9.35E-02		1.82E+01	1.82E+01		
HO	3.40E+06	3.39E+06	1.74E+04		4.70E+05		3.39E+06	3.39E+06		
HO+2	3.47E-04	3.46E-04	1.77E-06		1.77E-06		3.46E-04	3.46E-04		
HS-	8.26E+03	8.22E+03	4.22E+01		4.22E+01		8.22E+03	8.22E+03		
IA+3	1.89E+00	1.88E+00	9.64E-03		9.64E-03		1.88E+00	1.88E+00		
MD+2	2.55E+01	2.54E+01	1.30E-01		1.30E-01		2.54E+01	2.54E+01		
MN+4	8.05E+01	8.01E+01	4.11E-01		4.11E-01		8.01E+01	8.01E+01		
MD+6	1.09E+01	1.08E+01	5.56E-02		5.56E-02		1.08E+01	1.08E+01		
NA+	6.26E+05	6.23E+05	3.20E+03		3.20E+03		6.23E+05	6.23E+05		
NI+3	2.15E+00	2.14E+00	1.10E-02		1.10E-02		2.14E+00	2.14E+00		
NO2										
NO2-	2.32E+05	2.31E+05	1.19E+03		1.19E+03		2.31E+05	2.31E+05		
NO3-	4.85E+05	4.82E+05	2.47E+03		2.47E+03		4.82E+05	4.82E+05		
NO+4	6.32E-03	6.29E-03	3.22E-05		3.22E-05		6.29E-03	6.29E-03		
O2										
OH-	1.46E+05	1.45E+05	7.45E+02		7.45E+02		1.45E+05	1.45E+05		
PH+4	7.45E-02	7.41E-02	3.80E-04		3.80E-04		7.41E-02	7.41E-02		
PO4-3	1.27E+04	1.26E+04	6.48E+01		6.48E+01		1.26E+04	1.26E+04		
PU+4	2.06E-02	2.05E-02	1.05E-04		1.05E-04		2.05E-02	2.05E-02		
SE+6	1.16E-03	1.15E-03	5.91E-06		5.91E-06		1.15E-03	1.15E-03		
SI+4	5.59E+01	5.56E+01	2.85E-01		2.85E-01		5.56E+01	5.56E+01		
SN+4	1.26E-04	1.26E-04	6.44E-07		6.44E-07		1.26E-04	1.26E-04		
SO4-2	1.74E+04	1.73E+04	8.86E+01		8.86E+01		1.73E+04	1.73E+04		
SR+2	4.50E-02	4.48E-02	2.30E-04		2.30E-04		4.48E-02	4.48E-02		
TCO4-	2.40E+00	2.39E+00	1.23E-02		1.23E-02		2.39E+00	2.39E+00		
TI+4	2.93E-06	2.92E-06	1.29E-08		1.29E-08		2.92E-06	2.92E-06		
TCC	1.82E+04	1.81E+04	9.31E+01		9.31E+01		1.81E+04	1.81E+04		
UD+2	1.76E+01	1.75E+01	8.99E-02		8.99E-02		1.75E+01	1.75E+01		
ZN+2	4.22E+00	4.20E+00	2.15E-02		2.15E-02		4.20E+00	4.20E+00		
ZR+4	1.26E-04	1.26E-04	6.44E-07		6.44E-07		1.26E-04	1.26E-04		

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Table B-2 Phase 1 IAW Mass Balance for Batch PC1/2 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	5.38E+04	5.38E+02	5.33E+04		5.33E+04		5.38E+02	5.38E+02		
RADIOISOTOPES (Ci)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
BAO										
BBO										
BL2O3										
CaO										
CaO2										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
H2O										
HM2O										
K2O										
LA2O3										
MgO										
MNO2										
MCO3										
Na2O										
NIL2O3										
NI2O2										
PCO5										
PEO2										
PLO2										
SEO3										
STO2										
SN2O2										
SO3										
SULFURS	5.38E+04	5.38E+02	5.33E+04		5.33E+04		5.38E+02	5.38E+02		
SRO										
TC2O7										
TIO2										
U3O8										
ZNO										
ZNO2										

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Table B-2 Phase 1 LAW Mass Balance for Batch PCL/2 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.80E+06	3.27E+03		3.27E+03	3.80E+06	5.32E+06		1.00E-09	1.00E-09
Density (g/L)		1.41E+03	3.34E+03		3.34E+03	1.41E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		5.35E+06	1.09E+04		1.09E+04	5.35E+06	5.32E+06		1.00E-09	1.00E-09
RADIONUCLIDES (C1)										
Cesium		4.78E+03	5.61E+04		5.61E+04	4.78E+03				
Strontium		6.22E+03				6.22E+03				
Technetium		2.44E+01	2.48E-01		2.48E-01	2.44E+01				
TU		2.55E+00				2.55E+00				
CHEMICALS (kg)										
AG+		1.60E-01				1.60E-01				
AL(OH)4-		2.91E+05				2.91E+05				
AM+3		3.10E-04				3.10E-04				
AS+5		9.22E-02				9.22E-02				
Br+3		4.54E+00				4.54E+00				
BA+2		3.13E-01				3.13E-01				
BE+2		2.07E-02				2.07E-02				
BI+3		7.56E-05				7.56E-05				
C-14		1.46E-06				1.46E-06				
CA+2		2.91E+01				2.91E+01				
CD+2		1.17E-01				1.17E-01				
CL-		2.91E+04				2.91E+04				
CL2							2.91E+04			
CO3-2							1.27E+05			
CR(OH)4-		8.22E+04				8.22E+04				
CS+		2.43E+02				2.43E+02				
CSH		5.52E-02	6.48E-01		6.48E-01	5.52E-02				
CU+2		5.04E-06				5.04E-06				
EU-154		7.90E-10				7.90E-10				
F-		2.63E+04				2.63E+04				
F2							2.63E+04			
FE+3		1.82E+01				1.82E+01				
H2O		3.39E+06				3.39E+06		3.57E+06	1.00E-09	1.00E-09
HE+2		3.46E-04				3.46E-04				
HS-		8.22E+03				8.22E+03				
IA+3		1.88E+00				1.88E+00				
MD+2		2.54E+01				2.54E+01				
MN+4		8.01E+01				8.01E+01				
MO+6		1.08E+01				1.08E+01				
NA+		6.23E+05	6.26E+03		6.26E+03	6.23E+05				
NI+3		2.14E+00				2.14E+00				
NO2							5.89E+05			
NO2-		2.31E+05				2.31E+05				
NO3-		4.82E+05				4.82E+05				
NH4+		6.28E-03				6.28E-03				
O2							9.78E+05			
OH-		1.45E+05	4.64E+03		4.64E+03	1.45E+05				
PH4+		7.41E-02				7.41E-02				
PO4-3		1.26E+04				1.26E+04				
PU+4		2.05E-02				2.05E-02				
SE+6		1.15E-03				1.15E-03				
SI+4		5.56E+01				5.56E+01				
SN+4		1.26E-04				1.26E-04				
SO4-2		1.73E+04				1.73E+04				
SR+2		4.48E-02				4.48E-02				
TCO4-		2.37E+00	2.40E-02		2.40E-02	2.37E+00				
TI+4		2.52E-06				2.52E-06				
TCC		1.81E+04				1.81E+04				
UDC+2		1.75E+01				1.75E+01				
ZM+2		4.20E+00				4.20E+00				
ZR+4		1.26E-04				1.26E-04				

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Table B-2 Phase 1 IAW Mass Balance for Batch PCL/2 (6 sheets)

STREAM NAME SOLID COMPONENTS	11	12	13	14	15	16	16A	17	18	19
Total Mass Flow (kg)		5.38E+02		6.26E+03	6.26E+03	5.38E+02	1.03E+06			
RADIONUCLIDES (Ci)										
Cesium							4.78E+03			
Strontium							6.23E+03			
Technetium							2.44E+01			
TU1							2.54E+00			
CHEMICALS (kg)										
AC2O							1.72E-01			
AL2O3							1.56E+05			
AM2O3							3.41E-04			
AS2O5							1.42E-01			
B2O3							1.46E+01			
B4O							3.49E-01			
B2O							5.75E-02			
BI2O3							8.42E-05			
CaO							4.08E+01			
ClO							1.34E-01			
CR2O3							1.54E+02			
CS2O							5.84E-02			
CUO							6.31E-06			
EU2O3							9.15E-10			
FE2O3							2.61E+01			
FORMER										
H2O							3.73E-04			
HM2AT				6.26E+03	6.26E+03					
K2O							9.90E+03			
LA2O3							2.21E+00			
MO							4.21E+01			
MNO2							1.27E+02			
MCO3							1.63E+01			
NA2O							8.40E+05			
NI2O3							3.02E+00			
NI(O)							7.13E-03			
PO25							9.44E+03			
PR(O)							8.55E-02			
PL(O)							2.32E-02			
SE(O)							1.85E-03			
SI(O)							1.19E+02			
SN(O)							1.59E-04			
SO3							1.44E+04			
SULFIDS		5.38E+02				5.38E+02	5.38E+02			
SD							5.28E-02			
TC2O7							2.25E+00			
Ti(O)							4.20E-06			
U(O)							1.86E+01			
ZNO							5.22E+00			
ZRC(O)							1.70E-04			

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Table B-2 Phase 1 LAW Mass Balance for Batch PC1/2 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	5.32E+06				1.75E+06	3.57E+06	3.27E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	5.32E+06				1.75E+06	3.57E+06	1.09E+04	1.00E-09	1.00E+06
RADIONUCLIDES (C1)									
Cesium									
Strontium									
Technetium									
IU1									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
BH3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	2.91E+04				2.91E+04				
CL3	1.27E+05				1.27E+05				
CO3-2									
CR(OH)4-									
CS+									
CU+2									
EU-154									
F-									
F2	2.63E+04				2.63E+04				
FE+3									
H2O	3.57E+06					3.57E+06			
HG+2									
K+									
LA+3									
MC+2									
MN+4									
MO+6									
NA+							6.26E+03	5.75E-10	
NI+3									
NO2	5.89E+05				5.89E+05				
NO3-									
NE+4									
O2	9.78E+05				9.78E+05				1.00E+06
OH-									
EBH4							4.64E+03	4.25E-10	
EO4-3									
FU+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TDO+									
TI+4									
TCC									
TUC2+2									
ZN+2									
Zn+4									

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Table B-2 Phase 1 LAW Mass Balance for Batch PCL/2 (6 sheets)

STREAM NAME SOLID COMPONENTS	20	21	22	23	24	25	26	27	28
Total Mass Flow (kg)		1.03E+06	3.95E+06	4.98E+06					
RADIONUCLIDES (Cl)									
Cesium		4.78E+03		4.78E+03					
Strontium		6.23E+03		6.23E+03					
Technetium		2.44E+01		2.44E+01					
TU1		2.54E+00		2.54E+00					
CHEMICALS (kg)									
ACGD		1.72E-01		1.72E-01					
AL2O3		1.56E+05		1.56E+05					
AM2O3		3.41E-04		3.41E-04					
AS2O5		1.42E-01		1.42E-01					
B2O3		1.46E+01		1.46E+01					
B4O7		3.49E-01		3.49E-01					
BEO		5.73E-02		5.73E-02					
BL2O3		8.42E-05		8.42E-05					
CaO		4.08E+01		4.08E+01					
CaO		1.34E-01		1.34E-01					
CR2O3		1.54E+02		1.54E+02					
CS2O		5.84E-02		5.84E-02					
CUO		6.31E-06		6.31E-06					
EU2O3		9.15E-10		9.15E-10					
FE2O3		2.61E+01	3.95E+06	2.61E+01					
FORMER				3.95E+06					
H2O		3.73E-04		3.73E-04					
HM2AT									
H2O		9.90E+03		9.90E+03					
LA2O3		2.21E+00		2.21E+00					
MCO		4.21E+01		4.21E+01					
MNO2		1.27E+02		1.27E+02					
MCO3		1.63E+01		1.63E+01					
NA2O		8.40E+05		8.40E+05					
NIL2O3		3.02E+00		3.02E+00					
NEO2		7.13E-03		7.13E-03					
FE2O5		9.44E+03		9.44E+03					
FKO2		8.53E-02		8.53E-02					
FLU2		2.32E-02		2.32E-02					
SECO3		1.85E-03		1.85E-03					
SLIC2		1.19E+02		1.19E+02					
SNCO2		1.59E-04		1.59E-04					
SO3		1.44E+04		1.44E+04					
SOLIDS		5.38E+02		5.38E+02					
SFO		5.28E-02		5.28E-02					
TU2O7		2.23E+00		2.23E+00					
TIL2		4.20E-06		4.20E-06					
UO3		1.86E+01		1.86E+01					
ZNO		5.22E+00		5.22E+00					
ZRCO2		1.70E-04		1.70E-04					

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Table B-3 Phase 1 LAW Mass Balance for Batch PCL/3 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	2.38E+06	2.37E+06	1.16E+04	2.80E+05	2.92E+05		2.37E+06	2.37E+06		
Density (g/L)	1.40E+03	1.40E+03	1.40E+03	1.00E+03	1.02E+03		1.40E+03	1.40E+03		
Total Mass Flow (kg)	3.33E+06	3.31E+06	1.62E+04	2.80E+05	2.96E+05		3.31E+06	3.31E+06		
RADIONUCLIDES (Ci)										
Cesium	1.04E+06	1.04E+06	5.05E+03		5.05E+03		1.04E+06	1.04E+06		
Strontium	1.38E+04	1.37E+04	6.71E+01		6.71E+01		1.37E+04	1.37E+04		
Technetium	1.80E+02	1.79E+02	8.75E-01		8.75E-01		1.79E+02	1.79E+02		
IU1	1.65E+01	1.64E+01	7.99E-02		7.99E-02		1.64E+01	1.64E+01		
CHEMICALS (kg)										
AG+	7.48E-03	7.45E-03	3.63E-05		3.63E-05		7.45E-03	7.45E-03		
AL(OH)4-	1.94E+05	1.94E+05	9.44E+02		9.44E+02		1.94E+05	1.94E+05		
AM+3	6.20E-04	6.17E-04	3.01E-06		3.01E-06		6.17E-04	6.17E-04		
AS+5	4.34E-03	4.32E-03	2.11E-05		2.11E-05		4.32E-03	4.32E-03		
BA+3	2.13E-01	2.12E-01	1.03E-03		1.03E-03		2.12E-01	2.12E-01		
BE+2	1.47E-02	1.46E-02	7.13E-05		7.13E-05		1.46E-02	1.46E-02		
BE+2	9.59E-04	9.54E-04	4.66E-06		4.66E-06		9.54E-04	9.54E-04		
BI+3	3.53E-06	3.52E-06	1.72E-08		1.72E-08		3.52E-06	3.52E-06		
C-14	6.19E-08	6.16E-08	3.00E-10		3.00E-10		6.16E-08	6.16E-08		
CA+2	1.37E+00	1.36E+00	6.63E-03		6.63E-03		1.36E+00	1.36E+00		
CD+2	5.37E-03	5.34E-03	2.61E-05		2.61E-05		5.34E-03	5.34E-03		
CL-	1.17E+04	1.16E+04	5.66E+01		5.66E+01		1.16E+04	1.16E+04		
CL2										
CO2										
CO3-2	4.26E+04	4.24E+04	2.07E+02		2.07E+02		4.24E+04	4.24E+04		
CR(OH)4-	2.15E+03	2.14E+03	1.05E+01		1.05E+01		2.14E+03	2.14E+03		
CSH	1.20E+01	1.20E+01	5.83E-02		5.83E-02		1.20E+01	1.20E+01		
CU+2	2.36E-07	2.35E-07	1.15E-09		1.15E-09		2.35E-07	2.35E-07		
EU-154	3.70E-11	3.68E-11	1.80E-13		1.80E-13		3.68E-11	3.68E-11		
F-	1.23E+03	1.22E+03	5.96E+00		5.96E+00		1.22E+03	1.22E+03		
F2										
FE+3	1.62E+01	1.61E+01	7.85E-02	2.80E+05	7.85E-02		1.61E+01	1.61E+01		
FE20	2.12E+06	2.11E+06	1.03E+04		2.91E+05		2.11E+06	2.11E+06		
FE+2	1.62E-05	1.61E-05	7.85E-08		7.85E-08		1.61E-05	1.61E-05		
K+	1.02E+04	1.02E+04	4.95E+01		4.95E+01		1.02E+04	1.02E+04		
LA+3	8.81E-02	8.77E-02	4.28E-04		4.28E-04		8.77E-02	8.77E-02		
Mg+2	1.18E+00	1.18E+00	5.75E-03		5.75E-03		1.18E+00	1.18E+00		
MN+4	3.75E+00	3.73E+00	1.82E-02		1.82E-02		3.73E+00	3.73E+00		
MO+6	5.06E-01	5.04E-01	2.46E-03		2.46E-03		5.04E-01	5.04E-01		
NA+	4.07E+05	4.05E+05	1.98E+03		1.98E+03		4.05E+05	4.05E+05		
NI+3	9.83E-02	9.80E-02	4.78E-04		4.78E-04		9.80E-02	9.80E-02		
NO2										
NO3-	1.31E+05	1.31E+05	6.38E+02		6.38E+02		1.31E+05	1.31E+05		
NO3-	2.86E+05	2.85E+05	1.39E+03		1.39E+03		2.85E+05	2.85E+05		
NO3H4	2.94E-04	2.92E-04	1.43E-06		1.43E-06		2.92E-04	2.92E-04		
O2										
OH-	1.02E+05	1.02E+05	4.95E+02		4.95E+02		1.02E+05	1.02E+05		
OH4-	3.28E-03	3.26E-03	1.59E-05		1.59E-05		3.26E-03	3.26E-03		
IO4-3	4.42E+03	4.39E+03	2.14E+01		2.14E+01		4.39E+03	4.39E+03		
IU+4	1.98E-01	1.97E-01	9.60E-04		9.60E-04		1.97E-01	1.97E-01		
SE+6	5.38E-05	5.36E-05	2.61E-07		2.61E-07		5.36E-05	5.36E-05		
SI+4	2.60E+00	2.59E+00	1.26E-02		1.26E-02		2.59E+00	2.59E+00		
SM+2	5.89E-06	5.86E-06	2.86E-08		2.86E-08		5.86E-06	5.86E-06		
SO4-2	9.76E+03	9.72E+03	4.74E+01		4.74E+01		9.72E+03	9.72E+03		
SR+2	9.94E-02	9.89E-02	4.82E-04		4.82E-04		9.89E-02	9.89E-02		
TD2+	1.75E+01	1.74E+01	8.47E-02		8.47E-02		1.74E+01	1.74E+01		
TI+4	1.18E-07	1.18E-07	5.75E-10		5.75E-10		1.18E-07	1.18E-07		
TOC	7.16E+03	7.13E+03	3.48E+01		3.48E+01		7.13E+03	7.13E+03		
UD2+2	8.19E-01	8.16E-01	3.98E-03		3.98E-03		8.16E-01	8.16E-01		
ZN+2	1.97E-01	1.96E-01	9.57E-04		9.57E-04		1.96E-01	1.96E-01		
ZR+4	5.89E-06	5.86E-06	2.86E-08		2.86E-08		5.86E-06	5.86E-06		

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Table B-3 Phase 1 LAW Mass Balance for Batch PCL/3 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.33E+04	3.33E+02	3.29E+04		3.29E+04		3.33E+02	3.33E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AG2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
BL2O3										
CAO										
ClO										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
HO										
IMHAT										
K2O										
LA2O3										
NEO										
MNO2										
MCO3										
NA2O										
NI2O3										
NEO2										
PO25										
PR2O2										
PUO2										
SEB3										
SIC2										
SNO2										
SO3										
SULFIDS	3.33E+04	3.33E+02	3.29E+04		3.29E+04		3.33E+02	3.33E+02		
SRO										
TC2O7										
TIC2										
U3										
ZNO										
ZRC2										

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Table B-3 Phase 1 LAW Mass Balance for Batch PCL/3 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		2.37E+06	2.14E+03		2.14E+03	2.37E+06	3.64E+06		1.00E+09	1.00E+09
Density (g/L)		1.40E+03	3.32E+03		3.32E+03	1.40E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)										
		3.31E+06	7.09E+03		7.09E+03	3.31E+06	3.64E+06		1.00E+09	1.00E+09
RADIONUCLIDES (Ci)										
Cesium		3.10E+03	1.03E+06		1.03E+06	3.10E+03				
Strontium		1.37E+04				1.37E+04				
Technetium		1.78E+02	1.80E+00		1.80E+00	1.78E+02				
TBU		1.64E+01				1.64E+01				
CHEMICALS (kg)										
AO*		7.45E-03				7.45E-03				
AL(CH ₃) ₄ -		1.94E+05				1.94E+05				
AP*3		6.17E-04				6.17E-04				
AS*5		4.32E-03				4.32E-03				
BE*3		2.12E-01				2.12E-01				
BE*2		1.46E-02				1.46E-02				
BE*3		9.54E-04				9.54E-04				
BI*2		3.52E-06				3.52E-06				
C-14		6.16E-08				6.16E-08				
CA*2		1.36E+00				1.36E+00				
CD*2		5.34E-03				5.34E-03				
CL-		1.16E+04				1.16E+04				
CL2							1.16E+04			
CL3							5.72E+04			
Cl3-2		4.24E+04				4.24E+04				
CR(CH ₃) ₄ -		2.14E+03				2.14E+03				
CS*		3.58E-02	1.19E+01		1.19E+01	3.58E-02				
CH ₂		2.35E-07				2.35E-07				
EU-154		3.68E-11				3.68E-11				
F-		1.22E+03				1.22E+03				
F2							1.22E+03			
FE*3		1.61E+01				1.61E+01				
H2O		2.11E+06				2.11E+06		2.23E+06		
HG*2		1.61E-05				1.61E-05				
K*		1.02E+04				1.02E+04				
Li*3		8.77E-02				8.77E-02				
ME*2		1.18E+00				1.18E+00				
MN*4		3.73E+00				3.73E+00				
MD*6		5.04E-01				5.04E-01				
NA*		4.05E+05	4.07E+03		4.07E+03	4.05E+05				
NI*3		9.80E-02				9.80E-02				
NCO							3.42E+05			
NCO-		1.31E+05				1.31E+05				
NO3-		2.85E+05				2.85E+05				
NE*4		2.92E-04				2.92E-04				
O2							9.90E+05			
OH-		1.02E+05	3.01E+03		3.01E+03	1.02E+05				
EP*4		3.26E-03				3.26E-03				
EOA-3		4.39E+03				4.39E+03				
EU*4		1.97E-01				1.97E-01				
SE*6		5.36E-05				5.36E-05				
SI*4		2.59E+00				2.59E+00				
SN*4		5.86E-06				5.86E-06				
SOA-2		9.72E+03				9.72E+03				
SR*2		9.89E-02				9.89E-02				
TCD*4		1.72E+01				1.72E+01				
TI*4		1.18E-07				1.18E-07				
TIC		7.13E+03				7.13E+03				
UO ₂ *2		8.16E-01				8.16E-01				
ZN*2		1.96E-01				1.96E-01				
ZR*4		5.86E-06				5.86E-06				

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Table B-3 Phase 1 LAW Mass Balance for Batch PCL/3 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		3.33E+02		4.07E+03	4.07E+03	3.33E+02	6.75E+05			
RADIONUCLIDES (Ci)										
Cesium							3.10E+03			
Strontium							1.37E+04			
Technetium							1.78E+02			
TU							1.62E+01			
CHEMICALS (kg)										
Ag2O							8.00E-03			
Al2O3							1.04E+05			
AM2O3							6.78E-04			
AS2O5							6.62E-03			
B2O3							6.81E-01			
BaO							1.63E-02			
BaD							2.65E-03			
Bi2O3							3.92E-06			
CaO							1.90E+00			
CaD							6.10E-03			
CR2O3							1.36E+03			
CS2O							3.79E-02			
CUO							2.94E-07			
EU2O3							4.26E-11			
FE2O3							2.30E+01			
FORMER										
H2O							1.74E-05			
DMPT				4.07E+03	4.07E+03					
K2O							1.22E+04			
La2O3							1.03E-01			
MFO							1.95E+00			
MND2							5.91E+00			
MCO3							7.56E-01			
Na2O							5.46E+05			
NI2O3							1.38E-01			
NEO2							3.32E-04			
FO5							3.28E+03			
PHO2							3.76E-03			
PUO2							2.22E-01			
SEO3							8.61E-05			
SI02							5.54E+00			
SN02							7.45E-06			
SO3							8.10E+03			
SOLIDS		3.33E+02				3.33E+02	3.33E+02			
SFO							1.17E-01			
TC2O7							1.64E+01			
TiO2							1.97E-07			
UC3							8.64E-01			
ZNO							2.44E-01			
ZRO2							7.92E-06			

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Table B-3 Phase 1 LAW Mass Balance for Batch PCL/3 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	3.64E+06				1.40E+06	2.23E+06	2.12E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	3.64E+06				1.40E+06	2.23E+06	7.08E+03	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
B+3									
BE+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	1.16E+04				1.16E+04				
CL2	5.72E+04				5.72E+04				
CO3-2									
CR(OH)4-									
CS+									
Cl+2									
EJ-154									
F-									
F2	1.22E+03				1.22E+03				
FE+3									
H2O	2.23E+06					2.23E+06			
HM+2									
K+									
LA+3									
MD+2									
MH+4									
MD+6									
NA+							4.07E+03	5.75E-10	
NI+3									
NO2	3.42E+05				3.42E+05				
NO2-									
NO3-									
NO+4									
O2	9.90E+05				9.90E+05				1.00E+06
OH-									
EB+4							3.01E+03	4.25E-10	
EO4-3									
EU+4									
SE+6									
SI+4									
SN+4									
SD4-2									
SH+2									
TCD4-									
TI+4									
TCC									
UD2+2									
ZN+2									
ZR+4									

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Table B-3 Phase 1 LAW Mass Balance for Batch PCL/3 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		6.75E+05	2.56E+06	3.23E+06					
RADIONUCLIDES (CL)									
Cesium		3.10E+03		3.10E+03					
Strontium		1.37E+04		1.37E+04					
Technetium		1.78E+02		1.78E+02					
TRU		1.62E+01		1.62E+01					
CHEMICALS (kg)									
AG2O		8.00E-03		8.00E-03					
AL2O3		1.04E+05		1.04E+05					
AM2O3		6.78E-04		6.78E-04					
AS2O5		6.62E-03		6.62E-03					
EG2O		6.81E-01		6.81E-01					
FAO		1.63E-02		1.63E-02					
FD		2.63E-03		2.63E-03					
FI2O3		3.92E-06		3.92E-06					
GAO		1.90E+00		1.90E+00					
GEO		6.10E-03		6.10E-03					
GR2O3		1.36E+03		1.36E+03					
CS2O		3.79E-02		3.79E-02					
CUO		2.94E-07		2.94E-07					
EU2O3		4.26E-11		4.26E-11					
FE2O3		2.30E+01	2.56E+06	2.56E+06					
FURMER									
H2O		1.74E+05		1.74E+05					
EMHAT									
K2O		1.22E+04		1.22E+04					
LA2O3		1.03E-01		1.03E-01					
MG		1.95E+00		1.95E+00					
MNO2		5.91E+00		5.91E+00					
MCO3		7.56E-01		7.56E-01					
NA2O		5.46E+05		5.46E+05					
NI2O3		1.38E-01		1.38E-01					
NEO2		3.32E-04		3.32E-04					
PO5		3.28E+03		3.28E+03					
PKO2		3.76E-03		3.76E-03					
RUO2		2.23E-01		2.23E-01					
SEO3		8.61E-05		8.61E-05					
SiO2		5.54E+00		5.54E+00					
SN2O		7.45E-06		7.45E-06					
SO3		8.10E+03		8.10E+03					
SOLIDS		3.33E+02		3.33E+02					
SRO		1.17E-01		1.17E-01					
TC2O7		1.64E+01		1.64E+01					
TCO2		1.97E-07		1.97E-07					
UO3		8.64E-01		8.64E-01					
ZNO		2.44E-01		2.44E-01					
ZRC2		7.92E-06		7.92E-06					

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Table B-4 Phase 1 LAW Mass Balance for Batch PCL/4 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	2.63E+06	2.62E+06	1.34E+04	3.20E+05	3.34E+05		2.62E+06	2.62E+06		
Density (g/L)	1.45E+03	1.42E+03	1.45E+03	1.03E+03	1.02E+03		1.45E+03	1.45E+03		
Total Mass Flow (kg)	3.81E+06	3.79E+06	1.94E+04	3.20E+05	3.40E+05		3.79E+06	3.79E+06		
RADIONUCLIDES (Ci)										
Cesium	9.65E+05	9.60E+05	4.90E+03		4.90E+03		9.60E+05	9.60E+05		
Strontium	3.01E+03	3.03E+03	1.53E+01		1.53E+01		3.00E+03	3.00E+03		
Technetium	2.86E+02	2.83E+02	1.45E+00		1.45E+00		2.85E+02	2.85E+02		
IU	5.50E+00	5.47E+00	2.79E-02		2.79E-02		5.47E+00	5.47E+00		
CHEMICALS (kg)										
AGP	4.28E-04	4.26E-04	2.17E-06		2.17E-06		4.26E-04	4.26E-04		
AL(OH)4-	1.92E+05	1.91E+05	9.74E+02		9.74E+02		1.91E+05	1.91E+05		
AM#3	6.79E-04	6.76E-04	3.43E-06		3.43E-06		6.76E-04	6.76E-04		
AS#5	2.46E-04	2.47E-04	1.26E-06		1.26E-06		2.47E-04	2.47E-04		
BA#1	1.20E-02	1.20E-02	6.34E-05		6.34E-05		1.20E-02	1.20E-02		
BA#2	8.36E-04	8.32E-04	4.25E-06		4.25E-06		8.32E-04	8.32E-04		
BE#2	5.49E-05	5.46E-05	2.79E-07		2.79E-07		5.46E-05	5.46E-05		
BE#3	2.02E-07	2.01E-07	1.03E-09		1.03E-09		2.01E-07	2.01E-07		
C-14	1.50E-04	1.49E-04	7.59E-07		7.59E-07		1.49E-04	1.49E-04		
CA#2	5.99E+01	5.96E+01	3.04E-01		3.04E-01		5.96E+01	5.96E+01		
CD#2	3.05E-04	3.03E-04	1.52E-06		1.52E-06		3.03E-04	3.03E-04		
CL-	1.02E+04	1.01E+04	5.18E+01		5.18E+01		1.01E+04	1.01E+04		
CL2										
CO2										
CO3-2	2.54E+04	2.53E+04	1.29E+02		1.29E+02		2.53E+04	2.53E+04		
CR(OH)4-	8.35E+02	8.33E+02	4.24E+00		4.24E+00		8.30E+02	8.30E+02		
CSH	1.12E+01	1.11E+01	5.66E-02		5.66E-02		1.11E+01	1.11E+01		
CU#2	1.35E-08	1.34E-08	6.84E-11		6.84E-11		1.34E-08	1.34E-08		
EU-154	2.12E-12	2.11E-12	1.08E-14		1.08E-14		2.11E-12	2.11E-12		
F-	7.03E+01	7.00E+01	3.57E-01		3.57E-01		7.00E+01	7.00E+01		
F2										
FE#3	1.22E+00	1.21E+00	6.19E-03	3.20E+05	6.19E-03		1.21E+00	1.21E+00		
H2O	2.28E+06	2.27E+06	1.16E+04		3.32E+05		2.27E+06	2.27E+06		
HE#2	9.23E-07	9.20E-07	4.69E-09		4.69E-09		9.20E-07	9.20E-07		
HF	7.63E+04	7.59E+04	3.87E+02		3.87E+02		7.59E+04	7.59E+04		
LA#3	5.03E-03	5.00E-03	2.52E-05		2.52E-05		5.00E-03	5.00E-03		
ME#2	9.50E+01	9.46E+01	4.83E-01		4.83E-01		9.46E+01	9.46E+01		
MH#4	4.74E+01	4.71E+01	2.40E-01		2.40E-01		4.71E+01	4.71E+01		
MD#6	1.04E+02	1.03E+02	5.26E-01		5.26E-01		1.03E+02	1.03E+02		
NA#	4.46E+05	4.44E+05	2.26E+03		2.26E+03		4.44E+05	4.44E+05		
NI#3	5.62E-03	5.59E-03	2.85E-05		2.85E-05		5.59E-03	5.59E-03		
NO2										
NO2-	1.94E+05	1.93E+05	9.87E+02		9.87E+02		1.93E+05	1.93E+05		
NO3-	4.08E+05	4.06E+05	2.07E+03		2.07E+03		4.06E+05	4.06E+05		
NE#4	1.68E-05	1.67E-05	8.51E-08		8.51E-08		1.67E-05	1.67E-05		
O2										
OH-	1.63E+05	1.63E+05	8.29E+02		8.29E+02		1.63E+05	1.63E+05		
PH#4	5.47E+02	5.44E+02	2.78E+00		2.78E+00		5.44E+02	5.44E+02		
PO4-3	4.14E+03	4.12E+03	2.10E+01		2.10E+01		4.12E+03	4.12E+03		
PU#4	4.36E-02	4.36E-02	2.22E-04		2.22E-04		4.36E-02	4.36E-02		
SE#6	5.98E-02	5.95E-02	3.04E-04		3.04E-04		5.95E-02	5.95E-02		
SI#4	1.49E-01	1.48E-01	7.54E-04		7.54E-04		1.48E-01	1.48E-01		
SN#4	3.37E-07	3.35E-07	1.71E-09		1.71E-09		3.35E-07	3.35E-07		
SO4-2	2.59E+03	2.58E+03	1.32E+01		1.32E+01		2.58E+03	2.58E+03		
SR#2	2.17E-02	2.16E-02	1.10E-04		1.10E-04		2.16E-02	2.16E-02		
TD#4	2.77E+01	2.76E+01	1.41E-01		1.41E-01		2.76E+01	2.76E+01		
TI#4	8.55E+00	8.50E+00	4.34E-02		4.34E-02		8.50E+00	8.50E+00		
TCC	4.98E+03	4.95E+03	2.53E+01		2.53E+01		4.95E+03	4.95E+03		
UL#2	8.63E+02	8.59E+02	4.38E+00		4.38E+00		8.59E+02	8.59E+02		
ZH#2	5.70E+02	5.67E+02	2.90E+00		2.90E+00		5.67E+02	5.67E+02		
ZR#4	9.16E+01	9.11E+01	4.65E-01		4.65E-01		9.11E+01	9.11E+01		

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Table B-4 Phase 1 LAW Mass Balance for Batch PCL/4 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.81E+04	3.81E+02	3.77E+04		3.77E+04		3.81E+02	3.81E+02		
RADIOISOTOPES (Ci)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
H2O										
IMMRT										
K2O										
LA2O3										
MO										
MO2										
MO3										
Na2O										
NIL2O3										
NIP2										
PO2										
PO3										
PU2										
SE2O3										
SI2O2										
SO2										
SO3										
SOLIDS	3.81E+04	3.81E+02	3.77E+04		3.77E+04		3.81E+02	3.81E+02		
SrO										
TC2O7										
TI2O2										
U3O8										
ZNO										
ZrO2										

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Table B-4 Phase 1 LAW Mass Balance for Batch PCL/4 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		2.62E+06	2.34E+03		2.34E+03	2.62E+06	3.99E+06		1.00E+09	1.00E+09
Density (g/L)		1.45E+03	3.33E+03		3.33E+03	1.45E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		3.79E+06	7.77E+03		7.77E+03	3.79E+06	3.99E+06		1.00E+09	1.00E+09
RADIONUCLIDES (Ci)										
Cesium		3.40E+03	9.57E+05		9.57E+05	3.40E+03				
Strontium		3.00E+03				3.00E+03				
Technetium		2.82E+02	2.86E+00		2.86E+00	2.82E+02				
TU		5.47E+00				5.47E+00				
CHEMICALS (kg)										
AG+		4.26E-04				4.26E-04				
AL(OH)4-		1.91E+05				1.91E+05				
AM+3		6.76E-04				6.76E-04				
AS+5		2.47E-04				2.47E-04				
BA+3		1.20E-02				1.20E-02				
BA+2		8.32E-04				8.32E-04				
BE+3		5.46E-05				5.46E-05				
BI+3		2.01E-07				2.01E-07				
C-14		1.49E-04				1.49E-04				
CA+2		5.96E+01				5.96E+01				
CD+2		3.03E-04				3.03E-04				
CL-		1.01E+04				1.01E+04				
CL2							1.01E+04			
CL2							3.67E+04			
CO3-2		2.53E+04				2.53E+04				
CR(OH)4-		8.30E+02				8.30E+02				
CS+		3.93E-02	1.11E+01		1.11E+01	3.93E-02				
CH2		1.34E-08				1.34E-08				
EU-154		2.11E-12				2.11E-12				
F-		7.00E+01				7.00E+01				
F2							7.00E+01			
FE+3		1.21E+00				1.21E+00				
H2O		2.27E+06				2.27E+06	2.43E+06		1.00E+09	1.00E+09
H3+2		9.20E-07				9.20E-07				
K+		7.59E+04				7.59E+04				
LA+3		5.00E-03				5.00E-03				
MD+2		9.46E+01				9.46E+01				
MN+4		4.71E+01				4.71E+01				
MO+6		1.03E+02				1.03E+02				
NA+		4.44E+05	4.46E+03		4.46E+03	4.44E+05				
NI+3		5.59E-03				5.59E-03				
NO2							4.95E+05			
NO2-		1.93E+05				1.93E+05				
NO3-		4.06E+05				4.06E+05				
NE+4		1.67E-05				1.67E-05				
O2							1.02E+06			
OH-		1.63E+05	3.30E+03		3.30E+03	1.63E+05				
OH+		5.44E+02				5.44E+02				
FO4-3		4.12E+03				4.12E+03				
FU+4		4.36E-02				4.36E-02				
SE+6		5.92E-02				5.92E-02				
SI+4		1.48E-01				1.48E-01				
SN+4		3.35E-07				3.35E-07				
SD4-2		2.58E+03				2.58E+03				
SR+2		2.16E-02				2.16E-02				
TCD4-		2.73E+01	2.77E-01		2.77E-01	2.73E+01				
TI+4		8.50E+00				8.50E+00				
TCC		4.95E+03				4.95E+03				
UD2+2		8.59E+02				8.59E+02				
ZN+2		5.67E+02				5.67E+02				
ZN+4		9.11E+01				9.11E+01				

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Table B-4 Phase 1 LAW Mass Balance for Batch PCL/4 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		3.81E+02		4.46E+03	4.46E+03	3.81E+02	8.01E+05			
RADIONUCLIDES (Cl)										
Cesium							3.40E+03			
Strontium							3.00E+03			
Technetium							2.82E+02			
TU							5.44E+00			
CHEMICALS (kg)										
AG2O							4.57E-04			
AL2O3							1.02E+05			
AM2O3							7.43E-04			
AS2O5							3.78E-04			
B2O3							3.88E-02			
B4O							9.29E-04			
B2O							1.52E-04			
BI2O3							2.24E-07			
CaO							8.34E+01			
ClO							3.47E-04			
CR2O3							5.26E+02			
CS2O							4.16E-02			
CUO							1.68E-08			
EU2O3							2.44E-12			
FE2O3							1.73E+00			
FORMER										
H2O							9.93E-07			
IMHAT										
K2O				4.46E+03	4.46E+03					
LA2O3							9.14E+04			
M2O							5.87E-03			
M2O2							1.57E+02			
M2O2							7.45E+01			
MO3							1.55E+02			
NA2O							5.98E+05			
NI2O3							7.87E-03			
NEO2							1.89E-05			
EO5							3.08E+03			
FEO2							6.23E+02			
HUO2							4.94E-02			
SEB3							9.57E-02			
SI1O2							3.16E-01			
SN1O2							4.26E-07			
SO3							2.15E+03			
SOLIDS		3.81E+02				3.81E+02	3.81E+02			
SRO							2.54E-02			
TC2O7							2.60E+01			
TIO2							1.42E+01			
UO3							9.10E+02			
ZNO							7.06E+02			
ZRCO2							1.23E+02			

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Table B-4 Phase 1 LAW Mass Balance for Batch PCL/4 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	3.99E+06				1.56E+06	2.43E+06	2.33E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	3.99E+06				1.56E+06	2.43E+06	7.76E+03	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
BH+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	1.01E+04				1.01E+04				
CO2	3.67E+04				3.67E+04				
CO3-2									
CR(OH)4-									
CS+									
CI+2									
EU-154									
F-									
F2	7.00E+01				7.00E+01				
FE+3									
HEO	2.43E+06					2.43E+06			
HM+2									
K+									
LA+3									
MD+2									
MN+4									
MD+6									
NA+							4.46E+03	5.75E-10	
NI+3									
NO2	4.95E+05				4.95E+05				
NO2-									
NO3-									
NH+4									
O2	1.02E+06				1.02E+06				1.00E+06
OH-									
FBH+4							3.30E+03	4.25E-10	
EOA-3									
EU+4									
SE+6									
SI+4									
SNH+4									
SD+2									
SB+2									
TDO+4									
TI+4									
TCC									
UD+2									
ZN+2									
ZN+4									

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Table B-4 Phase 1 LAW Mass Balance for Batch PCL/4 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		8.01E+05	2.74E+06	3.54E+06					
RADIONUCLIDES (Ci)									
Cesium		3.40E+03		3.40E+03					
Strontium		3.00E+03		3.00E+03					
Technetium		2.82E+02		2.82E+02					
TRU		5.44E+00		5.44E+00					
CHEMICALS (kg)									
AG30		4.57E-04		4.57E-04					
AL2O3		1.02E+05		1.02E+05					
AM2O3		7.43E-04		7.43E-04					
AS2O5		3.78E-04		3.78E-04					
B2O3		3.88E-02		3.88E-02					
B4O7		9.29E-04		9.29E-04					
B2O		1.52E-04		1.52E-04					
Bi2O3		2.24E-07		2.24E-07					
CaO		8.34E+01		8.34E+01					
ClO		3.47E-04		3.47E-04					
CR2O3		5.26E+02		5.26E+02					
CS2O		4.16E-02		4.16E-02					
CUO		1.68E-08		1.68E-08					
EU2O3		2.44E-12		2.44E-12					
FE2O3		1.73E+00		1.73E+00					
FORMER			2.74E+06	2.74E+06					
H2O		9.93E-07		9.93E-07					
DMFAT									
K2O		9.14E+04		9.14E+04					
LA2O3		5.87E-03		5.87E-03					
MgO		1.57E+02		1.57E+02					
MNO2		7.45E+01		7.45E+01					
MCO3		1.55E+02		1.55E+02					
NA2O		5.98E+05		5.98E+05					
NI2O3		7.87E-03		7.87E-03					
NEO2		1.89E-05		1.89E-05					
P2O5		3.08E+03		3.08E+03					
PCO2		6.28E+02		6.28E+02					
PLU2		4.94E-02		4.94E-02					
SEO3		9.57E-02		9.57E-02					
STO2		3.16E-01		3.16E-01					
SNO2		4.26E-07		4.26E-07					
SO3		2.15E+03		2.15E+03					
SOLIDS		3.81E+02		3.81E+02					
SRO		2.54E-02		2.54E-02					
TC2O7		2.60E+01		2.60E+01					
TI02		1.42E+01		1.42E+01					
UO3		9.10E+02		9.10E+02					
ZNO		7.06E+02		7.06E+02					
ZrO2		1.23E+02		1.23E+02					

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Table B-5 Phase 1 LAW Mass Balance for Batch PCL/5 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.51E+06	3.49E+06	1.71E+04	4.16E+05	4.33E+05		3.49E+06	3.49E+06		
Density (g/L)	1.41E+03	1.41E+03	1.41E+03	1.00E+03	1.02E+03		1.41E+03	1.41E+03		
Total Mass Flow (kg)	4.93E+06	4.91E+06	2.41E+04	4.16E+05	4.40E+05		4.91E+06	4.91E+06		
RADIONUCLIDES (Ci)										
Cesium	1.34E+06	1.33E+06	6.55E+03		6.55E+03		1.33E+06	1.33E+06		
Strontium	2.22E+04	2.21E+04	1.09E+02		1.09E+02		2.21E+04	2.21E+04		
Technetium	3.08E+02	3.06E+02	1.50E+00		1.50E+00		3.06E+02	3.06E+02		
TbU	8.32E+00	8.28E+00	4.07E-02		4.07E-02		8.28E+00	8.28E+00		
CHEMICALS (kg)										
AG+	2.00E-05	2.00E-05	9.80E-08		9.80E-08		2.00E-05	2.00E-05		
AL(OH)4-	3.57E+05	3.55E+05	1.74E+03		1.74E+03		3.55E+05	3.55E+05		
AM+3	1.18E+03	1.18E+03	5.79E-06		5.79E-06		1.18E+03	1.18E+03		
ASH+5	1.17E-05	1.15E-05	5.70E-08		5.70E-08		1.16E-05	1.16E-05		
BH3	5.69E-04	5.67E-04	2.78E-06		2.78E-06		5.67E-04	5.67E-04		
BA+2	3.93E-05	3.91E-05	1.92E-07		1.92E-07		3.91E-05	3.91E-05		
BE+2	2.58E-06	2.56E-06	1.26E-08		1.26E-08		2.56E-06	2.56E-06		
BI+3	9.50E-09	9.46E-09	4.63E-11		4.63E-11		9.46E-09	9.46E-09		
C-14	7.70E-04	7.66E-04	3.76E-06		3.76E-06		7.66E-04	7.66E-04		
CA+2	1.50E+02	1.50E+02	7.35E-01		7.35E-01		1.50E+02	1.50E+02		
CD+2	2.71E+01	2.70E+01	1.33E-01		1.33E-01		2.70E+01	2.70E+01		
CL-	1.69E+04	1.69E+04	8.28E+01		8.28E+01		1.69E+04	1.69E+04		
CL2										
CO2										
CO3-2	1.69E+04	1.69E+04	8.28E+01		8.28E+01		1.69E+04	1.69E+04		
CR(OH)4-	3.37E+03	3.35E+03	1.65E+01		1.65E+01		3.35E+03	3.35E+03		
CS+	1.55E+01	1.54E+01	7.56E-02		7.56E-02		1.54E+01	1.54E+01		
CU+2	2.03E+01	2.02E+01	9.92E-02		9.92E-02		2.02E+01	2.02E+01		
F-	1.25E+03	1.25E+03	6.12E+00		6.12E+00		1.25E+03	1.25E+03		
F2										
FE+3	1.19E+02	1.19E+02	5.83E-01		5.83E-01		1.19E+02	1.19E+02		
EG2	3.16E+06	3.15E+06	1.53E+04	4.16E+05	4.31E+05		3.15E+06	3.15E+06		
HE+2	2.71E+01	2.70E+01	1.33E-01		1.33E-01		2.70E+01	2.70E+01		
K+	3.11E+04	3.10E+04	1.52E+02		1.52E+02		3.10E+04	3.10E+04		
LA+3	2.36E-04	2.33E-04	1.13E-06		1.13E-06		2.33E-04	2.33E-04		
MA+2	5.55E+01	5.52E+01	2.71E-01		2.71E-01		5.52E+01	5.52E+01		
MA+4	5.21E+01	5.18E+01	2.55E-01		2.55E-01		5.18E+01	5.18E+01		
MD+6	1.56E+02	1.56E+02	7.64E-01		7.64E-01		1.56E+02	1.56E+02		
NA+	6.00E+05	5.97E+05	2.93E+03		2.93E+03		5.97E+05	5.97E+05		
NI+3	4.06E+01	4.04E+01	1.99E-01		1.99E-01		4.04E+01	4.04E+01		
NO2										
NO2-	2.47E+05	2.46E+05	1.21E+03		1.21E+03		2.46E+05	2.46E+05		
NO3-	2.99E+05	2.98E+05	1.46E+03		1.46E+03		2.98E+05	2.98E+05		
NO+4	4.80E-02	4.78E-02	2.33E-04		2.33E-04		4.78E-02	4.78E-02		
O2										
OH-	1.76E+05	1.75E+05	8.61E+02		8.61E+02		1.75E+05	1.75E+05		
EB+4	1.61E+02	1.60E+02	7.85E-01		7.85E-01		1.60E+02	1.60E+02		
EO4-3	1.86E+03	1.85E+03	9.08E+00		9.08E+00		1.85E+03	1.85E+03		
EU+4	5.83E-02	5.80E-02	2.83E-04		2.83E-04		5.80E-02	5.80E-02		
SE+6	4.23E-03	4.20E-03	2.07E-05		2.07E-05		4.20E-03	4.20E-03		
SI+4	4.61E+02	4.58E+02	2.25E+00		2.25E+00		4.58E+02	4.58E+02		
SN+4	1.58E-08	1.57E-08	7.73E-11		7.73E-11		1.57E-08	1.57E-08		
SO4-2	2.88E+03	2.86E+03	1.41E+01		1.41E+01		2.86E+03	2.86E+03		
SR+2	1.60E-01	1.59E-01	7.81E-04		7.81E-04		1.59E-01	1.59E-01		
TCD+4	2.98E+01	2.97E+01	1.46E-01		1.46E-01		2.97E+01	2.97E+01		
TI+4	6.03E-01	6.00E-01	2.95E-03		2.95E-03		6.00E-01	6.00E-01		
TCC	1.28E+04	1.27E+04	6.25E+01		6.25E+01		1.27E+04	1.27E+04		
UC2+2	6.29E+01	6.26E+01	3.07E-01		3.07E-01		6.26E+01	6.26E+01		
WH6	3.53E+02	3.51E+02	1.72E+00		1.72E+00		3.51E+02	3.51E+02		
ZN+2	1.22E+02	1.21E+02	5.95E-01		5.95E-01		1.21E+02	1.21E+02		
ZR+4	6.45E+00	6.41E+00	3.15E-02		3.15E-02		6.41E+00	6.41E+00		

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Table B-5 Phase 1 LAW Mass Balance for Batch PCL/5 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.93E+04	4.93E+02	4.88E+04		4.88E+04		4.93E+02	4.93E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AG2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
BL2O3										
CaO										
CO										
CR2O3										
CS2O										
CUO										
FE2O3										
FORMER										
H2O										
INDIUM										
NO										
LA2O3										
MO										
MO2										
MO3										
Na2O										
NIL2O3										
NiO2										
P2O5										
PbO2										
PbO										
PO2										
SE2O3										
SiO2										
SnO2										
SO3										
SOLIDS	4.93E+04	4.93E+02	4.88E+04		4.88E+04		4.93E+02	4.93E+02		
SO										
Tc2O7										
TiO2										
UO3										
VO3										
ZNO										
ZrO2										

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Table B-5 Phase 1 LAW Mass Balance for Batch PCL/5 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.49E+06	3.14E+03		3.14E+03	3.49E+06	4.87E+06		1.00E-09	1.00E-09
Density (g/L)		1.41E+03	3.32E+03		3.32E+03	1.41E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.91E+06	1.05E+04		1.05E+04	4.91E+06	4.87E+06		1.00E-09	1.00E-09
RADIOISOTOPES (Ci)										
Cesium		4.57E+03	1.33E+06		1.33E+06	4.57E+03				
Sr-90		2.21E+04				2.21E+04				
Tc-99m		3.03E+02	3.08E+00		3.08E+00	3.03E+02				
TU		8.28E+00				8.28E+00				
CHEMICALS (kg)										
AC+		2.00E-05				2.00E-05				
AL(OH)4-		3.55E+05				3.55E+05				
AP+3		1.18E-03				1.18E-03				
AS+5		1.16E-05				1.16E-05				
BH3		5.67E-04				5.67E-04				
BA+2		3.91E-05				3.91E-05				
BE+2		2.56E-06				2.56E-06				
BI+3		9.46E-09				9.46E-09				
C-14		7.66E-04				7.66E-04				
CA+2		1.50E+02				1.50E+02				
CD+2		2.70E+01				2.70E+01				
CL-		1.69E+04				1.69E+04				
CL2							1.69E+04			
CO2							5.90E+04			
CO3-2		1.69E+04				1.69E+04				
CR(OH)4-		3.35E+03				3.35E+03				
CS+		5.28E-02	1.53E+01		1.53E+01	5.28E-02				
Cl+2		2.02E+01				2.02E+01				
F-		1.25E+03				1.25E+03				
F2							1.25E+03			
FE+3		1.19E+02				1.19E+02				
H2O		3.15E+06				3.15E+06	3.38E+06		1.00E-09	1.00E-09
H3+2		2.70E+01				2.70E+01				
K+		3.10E+04				3.10E+04				
LA+3		2.33E-04				2.33E-04				
MD+2		5.52E+01				5.52E+01				
MO+4		5.18E+01				5.18E+01				
MO+6		1.56E+02				1.56E+02				
NA+		5.97E+05	6.00E+03		6.00E+03	5.97E+05				
NI+3		4.04E+01				4.04E+01				
NO2							4.67E+05			
NO2-		2.46E+05				2.46E+05				
NO3-		2.98E+05				2.98E+05				
NO3+		4.78E-02				4.78E-02				
O2							9.46E+05			
OH-		1.75E+05	4.44E+03		4.44E+03	1.75E+05				
PH4		1.60E+02				1.60E+02				
PO4-3		1.85E+03				1.85E+03				
PU+4		5.80E-02				5.80E-02				
SE+6		4.20E-03				4.20E-03				
SI+4		4.58E+02				4.58E+02				
SN+4		1.57E-08				1.57E-08				
SO4-2		2.86E+03				2.86E+03				
SR+2		1.59E-01				1.59E-01				
TCO4-		2.94E+01	2.98E-01		2.98E-01	2.94E+01				
TI+4		6.00E-01				6.00E-01				
TCC		1.27E+04				1.27E+04				
UDC+2		6.26E+01				6.26E+01				
WH6		3.51E+02				3.51E+02				
ZN+2		1.21E+02				1.21E+02				
ZN+4		6.41E+00				6.41E+00				

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Table B-5 Phase 1 LAW Mass Balance for Batch PCL/5 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.93E+02		6.00E+03	6.00E+03	4.93E+02	1.04E+06			
RADIONUCLIDES (Ci)										
Cesium							4.57E+03			
Strontium							2.21E+04			
Technetium							3.03E+02			
TU							8.23E+00			
CHEMICALS (kg)										
AC2O							2.14E-05			
AL2O3							1.91E+05			
AM2O3							1.30E-03			
AS2O5							1.78E-05			
EG2O							1.82E-03			
BAO							4.37E-05			
BE2O							7.11E-06			
BI2O3							1.05E-08			
CAO							2.09E+02			
CO2							3.08E+01			
CR2O3							2.12E+03			
CS2O							5.59E-02			
CU2O							2.53E+01			
FE2O3							1.70E+02			
FORMER										
H2O							2.92E+01			
DMFAT										
K2O				6.00E+03	6.00E+03					
LA2O3							3.73E+04			
MG2O							2.75E-04			
MO2							9.15E+01			
MNO2							8.20E+01			
MCO3							2.34E+02			
NA2O							8.04E+05			
NI2O3							5.69E+01			
NEO2							5.43E-02			
EG2O5							1.38E+03			
FKO2							1.93E+02			
FLIO2							6.58E-02			
SE2O3							6.76E-03			
SI2O2							9.80E+02			
SNO2							2.00E-08			
SO3							2.39E+03			
SOLIDS		4.93E+02				4.93E+02				
SFO							1.87E-01			
TC2O7							2.79E+01			
TIO2							1.00E+00			
UO3							6.63E+01			
WO3							4.42E+02			
ZNO							1.51E+02			
ZRC2							8.66E+00			

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Table B-5 Phase I LAW Mass Balance for Batch PCL/5 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.87E+06				1.49E+06	3.38E+06	3.13E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	4.87E+06				1.49E+06	3.38E+06	1.04E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
Ag+									
Al(OH) ₄ ⁻									
Am ³⁺									
As ⁵⁺									
B ³⁺									
Ba ²⁺									
Be ²⁺									
Bi ³⁺									
C-14									
Ca ²⁺									
CD ²⁺									
Cl ⁻									
Cl ⁻²	1.69E+04				1.69E+04				
Cl ⁻²	5.90E+04				5.90E+04				
CO ₃ ⁻²									
Cr(OH) ₄ ⁻									
CS ⁺									
ClH ²⁺									
F ⁻									
F ₂	1.25E+03				1.25E+03				
Fe ³⁺									
H ₂ O	3.38E+06					3.38E+06			
Hg ²⁺									
K ⁺									
La ³⁺									
Mg ²⁺									
Mn ⁴⁺									
Mo ⁶⁺									
Na ⁺							6.00E+03	5.75E-10	
Ni ³⁺									
Ni ²⁺	4.67E+05				4.67E+05				
Ni ³⁺									
Ni ⁴⁺									
Cl ₂	9.46E+05				9.46E+05				
Cl ⁻									
ED ⁴⁺							4.44E+03	4.25E-10	
EO ₄ ⁻³									
Eu ⁴⁺									
Se ⁶⁺									
Si ⁴⁺									
Sn ⁴⁺									
SO ₄ ⁻²									
Sr ²⁺									
ICD ₄ ⁻									
Ti ⁴⁺									
Ti ³⁺									
UO ₂ ²⁺									
U ⁶⁺									
Zn ²⁺									
Zr ⁴⁺									

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Table B-5 Phase 1 LAW Mass Balance for Batch PCL/5 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		1.04E+06	3.72E+06	4.76E+06					
RADIONUCLIDES (Cl)									
Cesium		4.57E+03		4.57E+03					
Strontium		2.21E+04		2.21E+04					
Technetium		3.03E+02		3.03E+02					
Iru		8.23E+00		8.23E+00					
CHEMICALS (kg)									
AC2O		2.14E-05		2.14E-05					
AL2O3		1.91E+05		1.91E+05					
AM2O3		1.30E-03		1.30E-03					
AS2O5		1.78E-05		1.78E-05					
BC2O		1.82E-03		1.82E-03					
BAO		4.37E-05		4.37E-05					
BB		7.11E-06		7.11E-06					
BL2O3		1.03E-08		1.03E-08					
CAO		2.09E+02		2.09E+02					
ClO		3.08E+01		3.08E+01					
CR2O3		2.12E+03		2.12E+03					
CS2O		5.59E-02		5.59E-02					
CUO		2.53E+01		2.53E+01					
FE2O3		1.70E+02		1.70E+02					
FORMER			3.72E+06						
HEO		2.92E+01		2.92E+01					
DMAT									
K2O		3.73E+04		3.73E+04					
LA2O3		2.75E-04		2.75E-04					
NO		9.15E+01		9.15E+01					
NO2		8.20E+01		8.20E+01					
NCO3		2.34E+02		2.34E+02					
NA2O		8.04E+05		8.04E+05					
NL2O3		5.69E+01		5.69E+01					
NFCO		5.43E-02		5.43E-02					
FAO5		1.38E+03		1.38E+03					
EBO2		1.85E+02		1.85E+02					
FUCO2		6.58E-02		6.58E-02					
SEBO		6.76E-03		6.76E-03					
STO2		9.80E+02		9.80E+02					
SHO2		2.00E-08		2.00E-08					
SO3		2.39E+03		2.39E+03					
SOLIDS		4.93E+02		4.93E+02					
SFO		1.87E-01		1.87E-01					
TC2O7		2.79E+01		2.79E+01					
TI02		1.00E+00		1.00E+00					
UCO		6.63E+01		6.63E+01					
WCO		4.42E+02		4.42E+02					
ZNO		1.51E+02		1.51E+02					
ZCO2		8.66E+00		8.66E+00					

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Table B-6 Phase 1 LAW Mass Balance for Batch PCL/6 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	1.06E+06	1.05E+06	6.83E+03	1.13E+05	1.20E+05		1.05E+06	1.05E+06		
Density (g/L)	1.29E+03	1.29E+03	1.29E+03	1.00E+03	1.02E+03		1.29E+03	1.29E+03		
Total Mass Flow (kg)	1.37E+06	1.36E+06	8.83E+03	1.13E+05	1.22E+05		1.36E+06	1.36E+06		
RADIOISOTOPES (Ci)										
Cesium	1.77E+06	1.75E+06	1.14E+04		1.14E+04		1.75E+06	1.75E+06		
Strontium	4.47E+03	4.44E+03	2.89E+01		2.89E+01		4.44E+03	4.44E+03		
Technetium	3.53E+02	3.53E+02	2.30E+00		2.30E+00		3.53E+02	3.53E+02		
IU	3.48E+01	3.46E+01	2.25E-01		2.25E-01		3.46E+01	3.46E+01		
CHEMICALS (kg)										
Ag+	6.11E-07	6.07E-07	3.95E-09		3.95E-09		6.07E-07	6.07E-07		
Al(OH) ₃	4.01E+04	3.98E+04	2.60E+02		2.60E+02		3.98E+04	3.98E+04		
Am+3	5.56E-03	5.52E-03	3.60E-05		3.60E-05		5.52E-03	5.52E-03		
As+5	3.53E-07	3.51E-07	2.29E-09		2.29E-09		3.51E-07	3.51E-07		
BH3	1.74E-05	1.73E-05	1.12E-07		1.12E-07		1.73E-05	1.73E-05		
Br+2	4.65E-02	4.62E-02	3.73E-04		3.73E-04		4.62E-02	4.62E-02		
Br+2	7.81E-08	7.76E-08	5.06E-10		5.06E-10		7.76E-08	7.76E-08		
Br+3	2.89E-10	2.87E-10	1.87E-12		1.87E-12		2.87E-10	2.87E-10		
C-14	4.24E-04	4.22E-04	2.75E-06		2.75E-06		4.22E-04	4.22E-04		
Ca+2	8.81E+00	8.76E+00	5.70E-02		5.70E-02		8.76E+00	8.76E+00		
Ca+2	1.30E+00	1.29E+00	8.39E-03		8.39E-03		1.29E+00	1.29E+00		
Cl-	9.25E+02	9.19E+02	5.98E+00		5.98E+00		9.19E+02	9.19E+02		
Cl2										
CO2										
CO3-2	3.76E+04	3.73E+04	2.43E+02		2.43E+02		3.73E+04	3.73E+04		
CR(OH) ₃	2.46E+03	2.43E+03	1.59E+01		1.59E+01		2.43E+03	2.43E+03		
CS+	2.04E+01	2.03E+01	1.32E-01		1.32E-01		2.03E+01	2.03E+01		
ClH2	9.68E-01	9.61E-01	6.26E-03		6.26E-03		9.61E-01	9.61E-01		
EU-154	1.02E-02	1.01E-02	6.60E-05		6.60E-05		1.01E-02	1.01E-02		
F-	1.74E+03	1.73E+03	1.12E+01		1.12E+01		1.73E+03	1.73E+03		
F2										
FEH3	5.78E+00	5.74E+00	3.74E-02	1.13E+05	3.74E-02		5.74E+00	5.74E+00		
H2O	9.68E+05	9.61E+05	6.26E+03		6.26E+03		9.61E+05	9.61E+05		
Hg+2	1.30E+00	1.29E+00	8.39E-03		8.39E-03		1.29E+00	1.29E+00		
K+	4.23E+03	4.21E+03	2.74E+01		2.74E+01		4.21E+03	4.21E+03		
LAH3	4.99E-01	4.96E-01	3.23E-03		3.23E-03		4.96E-01	4.96E-01		
MEH2	2.68E+00	2.66E+00	1.73E-02		1.73E-02		2.66E+00	2.66E+00		
MH4	2.45E+00	2.44E+00	1.59E-02		1.59E-02		2.44E+00	2.44E+00		
MDH6	7.38E+00	7.33E+00	4.78E-02		4.78E-02		7.33E+00	7.33E+00		
NA+	1.25E+05	1.25E+05	8.11E+02		8.11E+02		1.25E+05	1.25E+05		
NIH3	2.45E+00	2.44E+00	1.59E-02		1.59E-02		2.44E+00	2.44E+00		
NO2										
NO2-	6.71E+04	6.67E+04	4.35E+02		4.35E+02		6.67E+04	6.67E+04		
NO3-	7.40E+04	7.36E+04	4.79E+02		4.79E+02		7.36E+04	7.36E+04		
NEH4	1.05E-01	1.05E-01	6.82E-04		6.82E-04		1.05E-01	1.05E-01		
O2										
OH-	1.74E+04	1.73E+04	1.12E+02		1.12E+02		1.73E+04	1.73E+04		
PH4	7.22E+00	7.18E+00	4.68E-02		4.68E-02		7.18E+00	7.18E+00		
PO4-3	1.01E+03	1.00E+03	6.54E+00		6.54E+00		1.00E+03	1.00E+03		
PUH4	2.16E-01	2.15E-01	1.40E-03		1.40E-03		2.15E-01	2.15E-01		
SEH6	1.53E-04	1.52E-04	9.90E-07		9.90E-07		1.52E-04	1.52E-04		
SIH4	3.28E+02	3.25E+02	2.12E+00		2.12E+00		3.25E+02	3.25E+02		
SNH4	4.80E-10	4.77E-10	3.11E-12		3.11E-12		4.77E-10	4.77E-10		
SO4-2	2.08E+04	2.07E+04	1.35E+02		1.35E+02		2.07E+04	2.07E+04		
SR+2	3.21E-02	3.19E-02	2.08E-04		2.08E-04		3.19E-02	3.19E-02		
TIO4-	3.44E+01	3.42E+01	2.23E-01		2.23E-01		3.42E+01	3.42E+01		
TIH4	2.19E-02	2.17E-02	1.42E-04		1.42E-04		2.17E-02	2.17E-02		
TCC	2.26E+03	2.25E+03	1.47E+01		1.47E+01		2.25E+03	2.25E+03		
UCO+2	1.90E+03	1.89E+03	1.23E+01		1.23E+01		1.89E+03	1.89E+03		
WH6	1.69E+01	1.67E+01	1.09E-01		1.09E-01		1.67E+01	1.67E+01		
ZNH2	5.44E+00	5.40E+00	3.52E-02		3.52E-02		5.40E+00	5.40E+00		
ZNH4	2.33E-01	2.32E-01	1.51E-03		1.51E-03		2.32E-01	2.32E-01		

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Table B-6 Phase 1 LAW Mass Balance for Batch PCL/6 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	1.37E+04	1.37E+02	1.35E+04		1.35E+04		1.37E+02	1.37E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
AG2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
EL2O3										
FE2O3										
FORMER										
HEO										
DMAT										
KG										
LA2O3										
MO										
MO2										
MO3										
NA2O										
NL2O3										
NEO2										
PEO5										
PHO2										
PUO2										
SDO3										
SiO2										
SN2										
SO3										
SOLIDS	1.37E+04	1.37E+02	1.35E+04		1.35E+04		1.37E+02	1.37E+02		
SRO										
TU2O7										
TiO2										
UO3										
VO3										
ZNO										
ZK2										

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Table B-6 Phase 1 LAW Mass Balance for Batch PCL/6 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		1.05E+06	6.74E+02		6.74E+02	1.05E+06	2.14E+06	6.64E+02	1.25E+03	1.92E+03
Density (g/L)		1.29E+03	3.27E+03		3.27E+03	1.29E+03	1.00E+03	3.30E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)		1.36E+06	2.20E+03		2.20E+03	1.36E+06	2.14E+06	2.19E+03	1.25E+03	3.44E+03
RADIOISOTOPES (Ci)										
Cesium		2.39E+03	1.75E+06		1.75E+06	2.39E+03				
Strontium		4.44E+03				4.44E+03				
Technetium		3.49E+02	3.55E+00		3.55E+00	2.39E+02		1.10E+02		1.10E+02
TU		3.46E+01				3.46E+01				
CHEMICALS (kg)										
AG+		6.07E-07				6.07E-07				
AL(CH) ₄ -		3.98E+04				3.98E+04				
AM#3		5.52E-03				5.52E-03				
AM#5		3.51E-07				3.51E-07				
BM#3		1.73E-05				1.73E-05				
BM#2		4.65E-02				4.65E-02				
BM#1		7.76E-08				7.76E-08				
BT#3		2.87E-10				2.87E-10				
C-14		4.22E-04				4.22E-04				
CA#2		8.76E+00				8.76E+00				
CD#2		1.29E+00				1.29E+00				
CL-		9.19E+02				9.19E+02				
CL2								9.19E+02		
CO2								3.56E+04		
CO3-2		3.73E+04				3.73E+04				
CR(CH) ₄ -		2.43E+03				2.43E+03				
CS+		2.76E-02	2.02E+01		2.02E+01	2.76E-02				
CU#2		9.61E-01				9.61E-01				
EU-154		1.01E-02				1.01E-02				
F-		1.73E+03				1.73E+03				
F2								1.73E+03		
FE#3		5.74E+00				5.74E+00				
H2O		9.61E+05				9.61E+05	9.86E+05		1.25E+03	1.25E+03
HG#2		1.29E+00				1.29E+00				
IC+		4.21E+03				4.21E+03				
IA#3		4.96E-01				4.96E-01				
IE#2		2.66E+00				2.66E+00				
IN#4		2.44E+00				2.44E+00				
ND#6		7.33E+00				7.33E+00				
NI+		1.25E+05	1.25E+03		1.25E+03	1.25E+05		1.25E+03		1.25E+03
NI#3		2.44E+00				2.44E+00				
NO2								1.21E+05		
NO2-		6.67E+04				6.67E+04				
NO3-		7.36E+04				7.36E+04				
NE#4		1.05E-01				1.05E-01				
O2								9.94E+05		
OH-		1.73E+04	9.27E+02		9.27E+02	1.73E+04		9.27E+02		9.27E+02
EB#4		7.18E+00				7.18E+00				
FD#-3		1.00E+03				1.00E+03				
FI#4		2.15E-01				2.15E-01				
SE#6		1.52E-04				1.52E-04				
SI#4		3.25E+02				3.25E+02				
SN#4		4.77E-10				4.77E-10				
SO#-2		2.07E+04				2.07E+04				
SR#2		3.19E-02				3.19E-02		1.07E+01		
TDO#-		3.39E+01	3.44E-01		3.44E-01	2.31E+01				1.07E+01
TI#4		2.17E-02				2.17E-02				
TCC		2.25E+03				2.25E+03				
UD#2		1.89E+03				1.89E+03				
WH6		1.67E+01				1.67E+01				
ZH#2		5.40E+00				5.40E+00				
ZR#4		2.32E-01				2.32E-01				

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Table B-6 Phase 1 LAW Mass Balance for Batch PCL/6 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		1.37E+02		1.25E+03	1.25E+03	1.37E+02	2.17E+05			
RADIONUCLIDES (Ci)										
Cesium							2.39E+03			
Strontium							4.44E+03			
Technetium							2.39E+02			
TU							3.44E+01			
CHEMICALS (kg)										
AC2O							6.52E-07			
AL2O3							2.14E+04			
AM2O3							6.07E-03			
AS2O5							5.39E-07			
B2O3							5.56E-05			
B4O							5.20E-02			
B2O							2.15E-07			
BL2O3							3.20E-10			
CaO							1.23E+01			
ClO							1.47E+00			
CR2O3							1.55E+03			
CS2O							2.92E-02			
CU							1.20E+00			
EU2O3							1.17E-02			
FE2O3							8.21E+00			
FORMER										
H2O							1.39E+00			
HMPT										
K2O				1.25E+03	1.25E+03					
La2O3							5.07E+03			
MO							5.82E-01			
MO3							4.41E+00			
MO2							3.86E+00			
HCO3							1.10E+01			
Na2O							1.68E+05			
NI2O3							3.43E+00			
NEO2							1.19E-01			
Fe2O5							7.51E+02			
FeO2							8.29E+00			
Flu2							2.44E-01			
SiO3							2.44E-04			
SiO2							6.96E+02			
SiO2							6.06E-10			
SO3							1.72E+04			
SOLIDS		1.37E+02					1.37E+02			
SrO							3.76E-02			
TU2O7							2.20E+01			
TiO2							3.62E-02			
UO3							2.00E+03			
WO3							2.11E+01			
ZNO							6.72E+00			
ZrO2							3.13E-01			

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Table B-6 Phase 1 LAW Mass Balance for Batch PCL/6 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	2.14E+06				1.15E+06	9.86E+05	6.54E+02	6.54E+02	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	2.14E+06				1.15E+06	9.86E+05	2.18E+03	2.18E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AGP									
AL(OH)4-									
AM+3									
AS+5									
BH+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	9.19E+02				9.19E+02				
CO2	3.56E+04				3.56E+04				
CO3-2									
CR(OH)4-									
CS+									
CH2									
EU-154									
F-									
F2	1.73E+03				1.73E+03				
FE+3						9.86E+05			
H2O	9.86E+05								
H3+2									
K+									
LA+3									
NE+2									
MH+4									
MD+6									
NA+							1.25E+03	1.25E+03	
NI+3									
NO2	1.21E+05				1.21E+05				
NO2-									
NO3-									
NE+4									
O2	9.94E+05				9.94E+05				1.00E+06
OH-							9.27E+02	9.27E+02	
EB+4									
EO4-3									
EU+4									
SE+6									
SI+4									
SN+4									
SD4-2									
SR+2									
TIO4-									
TI+4									
TCC									
UC2+2									
WH6									
ZN+2									
ZR+4									

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Table B-6 Phase 1 LAW Mass Balance for Batch PCL/6 (6 sheets)

STREAM NAME SOLID COMPONENTS	20	21	22	23	24	25	26	27	28
Total Mass Flow (kg)		2.17E+05	2.27E+06	2.49E+06					
RADIONUCLIDES (Cl)									
Cesium		2.39E+03		2.39E+03					
Strontium		4.44E+03		4.44E+03					
Technetium		2.39E+02		2.39E+02					
TU		3.44E+01		3.44E+01					
CHEMICALS (kg)									
ACSO		6.52E-07		6.52E-07					
AL2O3		2.14E+04		2.14E+04					
AM2O3		6.07E-03		6.07E-03					
AS2O5		5.39E-07		5.39E-07					
B2O3		5.56E-05		5.56E-05					
B4O		5.20E-02		5.20E-02					
BBO		2.15E-07		2.15E-07					
BL2O3		3.20E-10		3.20E-10					
CaO		1.23E+01		1.23E+01					
ClO		1.47E+00		1.47E+00					
CR2O3		1.55E+03		1.55E+03					
CS2O		2.92E-02		2.92E-02					
CUO		1.20E+00		1.20E+00					
EU2O3		1.17E-02		1.17E-02					
FE2O3		8.21E+00		8.21E+00					
FORMER			2.27E+06	2.27E+06					
H2O		1.39E+00		1.39E+00					
IMMAT									
K2O		5.07E+03		5.07E+03					
LA2O3		5.82E-01		5.82E-01					
MO		4.41E+00		4.41E+00					
MO2		3.86E+00		3.86E+00					
MO3		1.10E+01		1.10E+01					
NA2O		1.68E+05		1.68E+05					
NIL2O3		3.43E+00		3.43E+00					
NEO2		1.19E-01		1.19E-01					
PE2O5		7.51E+02		7.51E+02					
PF2O2		8.29E+00		8.29E+00					
RU2O2		2.44E-01		2.44E-01					
SE2O3		2.44E-04		2.44E-04					
SI2O2		6.96E+02		6.96E+02					
SMO2		6.06E-10		6.06E-10					
SO3		1.72E+04		1.72E+04					
SOLIDS		1.37E+02		1.37E+02					
SPO		3.76E-02		3.76E-02					
TC2O7		2.20E+01		2.20E+01					
TI2O2		3.62E-02		3.62E-02					
UO3		2.00E+03		2.00E+03					
VO3		2.11E+01		2.11E+01					
ZNO		6.72E+00		6.72E+00					
ZR2O2		3.13E-01		3.13E-01					

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Table B-7 Phase 1 LAW Mass Balance for Batch PCL/7 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	7.51E+05	7.47E+05	3.66E+03	8.30E+04	8.66E+04		7.47E+05	7.47E+05	3.66E+03	8.36E+02
Density (g/L)	1.31E+03	1.31E+03	1.31E+03	1.00E+03	1.01E+03		1.31E+03	1.31E+03	1.31E+03	1.00E+03
Total Mass Flow (kg)	9.86E+05	9.81E+05	4.80E+03	8.30E+04	8.78E+04		9.81E+05	9.81E+05	4.84E+01	8.36E+02
RADIONUCLIDES (Ci)										
Cesium	3.14E+05	3.12E+05	1.53E+03		1.53E+03		3.12E+05	3.12E+05	1.54E+01	
Strontium	4.46E+04	4.46E+04	2.18E+02		2.18E+02		5.72E+03	5.72E+03	2.82E-01	
Technetium	1.87E+02	1.86E+02	9.13E-01		9.13E-01		1.86E+02	1.86E+02	9.19E-03	
TRU	3.20E+02	3.19E+02	1.56E+00		1.56E+00		8.11E+01	8.11E+01	4.00E-03	
CHEMICALS (kg)										
AG+	5.20E-08	5.18E-08	2.53E-10		2.53E-10		5.18E-08	5.18E-08	2.53E-12	
AL(OH)4-	6.09E+03	6.06E+03	2.97E+01		2.97E+01		6.06E+03	6.06E+03	2.99E-01	
AsH3	8.81E-02	8.77E-02	4.29E-04		4.29E-04		2.23E-02	2.23E-02	1.10E-06	
AsH5	3.01E-08	2.99E-08	1.47E-10		1.47E-10		2.99E-08	2.99E-08	1.46E-12	
BH3	1.46E-06	1.47E-06	7.20E-09		7.20E-09		1.47E-06	1.47E-06	7.23E-11	
BH2	5.03E-03	5.03E-03	2.43E-05		2.43E-05		5.03E-03	5.03E-03	2.43E-07	
BEH2	6.65E-09	6.62E-09	3.24E-11		3.24E-11		6.62E-09	6.62E-09	3.26E-13	
BIH3	2.45E-11	2.44E-11	1.20E-13		1.20E-13		2.44E-11	2.44E-11	1.20E-15	
C-14	4.50E-05	4.48E-05	2.19E-07		2.19E-07		4.48E-05	4.48E-05	2.21E-09	
CaH2	2.65E+02	2.64E+02	1.29E+00		1.29E+00		2.64E+02	2.64E+02	1.30E-02	
CDH2	1.21E-01	1.20E-01	5.89E-04		5.89E-04		1.20E-01	1.20E-01	5.93E-06	
CL-	1.58E+03	1.57E+03	7.70E+00		7.70E+00		1.57E+03	1.57E+03	7.76E-02	
CL2										
CO3-2										
CO3-2	4.01E+04	3.99E+04	1.95E+02		1.95E+02		3.99E+04	3.99E+04	1.97E+00	
CSH(OH)4-	4.51E+02	4.49E+02	2.20E+00		2.20E+00		4.49E+02	4.49E+02	2.21E-02	
CSH	3.62E+00	3.60E+00	1.76E-02		1.76E-02		3.60E+00	3.60E+00	1.78E-04	
ClH2	9.07E-02	9.03E-02	4.42E-04		4.42E-04		9.03E-02	9.03E-02	4.43E-06	
EU-154	1.10E-03	1.09E-03	5.35E-06		5.35E-06		1.09E-03	1.09E-03	5.38E-08	
F-	1.86E+02	1.85E+02	9.05E-01		9.05E-01		1.85E+02	1.85E+02	9.11E-03	
F2										
FEH3	7.21E+02	7.18E+02	3.52E+00		3.52E+00		7.18E+02	7.18E+02	3.54E-02	
H2O	6.21E+05	6.18E+05	3.03E+03	8.30E+04	8.60E+04		6.18E+05	6.18E+05	3.03E+01	8.36E+02
H2O2	1.21E-01	1.20E-01	5.89E-04		5.89E-04		1.20E-01	1.20E-01	5.93E-06	
K+	1.45E+03	1.44E+03	7.07E+00		7.07E+00		1.44E+03	1.44E+03	7.12E-02	
LAH3	5.37E-02	5.34E-02	2.61E-04		2.61E-04		5.34E-02	5.34E-02	2.63E-06	
MH2	2.51E-01	2.49E-01	1.22E-03		1.22E-03		2.49E-01	2.49E-01	1.23E-05	
MH4	2.41E+02	2.40E+02	1.17E+00		1.17E+00		2.40E+02	2.40E+02	1.18E-02	
MDH6	6.87E-01	6.84E-01	3.35E-03		3.35E-03		6.84E-01	6.84E-01	3.37E-05	
Na+	1.20E+05	1.20E+05	5.85E+02		5.85E+02		1.20E+05	1.20E+05	5.89E+00	
NI+3	2.17E+02	2.16E+02	1.06E+00		1.06E+00		2.16E+02	2.16E+02	1.06E-02	
NO2										
NO2-	3.06E+04	3.06E+04	1.50E+02		1.50E+02		3.06E+04	3.06E+04	1.51E+00	
NO3-	1.22E+05	1.21E+05	5.94E+02		5.94E+02		1.21E+05	1.21E+05	5.98E+00	
NO3+	1.13E-02	1.13E-02	5.51E-05		5.51E-05		1.13E-02	1.13E-02	5.53E-07	
O2										
OH-	1.04E+04	1.03E+04	5.05E+01		5.05E+01		1.03E+04	1.03E+04	5.09E-01	
OH2	1.59E+02	1.58E+02	7.75E-01		7.75E-01		1.58E+02	1.58E+02	7.80E-03	
FO4-3	3.62E+02	3.60E+02	1.76E+00		1.76E+00		3.60E+02	3.60E+02	1.78E-02	
FU4	2.48E-01	2.46E-01	1.21E-03		1.21E-03		6.29E-02	6.29E-02	3.10E-06	
SEH6	1.36E-05	1.35E-05	6.61E-08		6.61E-08		1.35E-05	1.35E-05	6.66E-10	
SIH4	3.49E+01	3.47E+01	1.70E-01		1.70E-01		3.47E+01	3.47E+01	1.71E-03	
SNH4	4.10E-11	4.08E-11	2.00E-13		2.00E-13		4.08E-11	4.08E-11	2.01E-15	
SD4-2	8.81E+03	8.77E+03	4.29E+01		4.29E+01		8.77E+03	8.77E+03	4.32E-01	
SH2	3.22E-01	3.21E-01	1.57E-03		1.57E-03		4.11E-02	4.11E-02	2.03E-06	
TDH+	1.61E+01	1.61E+01	8.84E-02		8.84E-02		1.61E+01	1.61E+01	8.90E-04	
TIH4	1.94E-03	1.93E-03	9.43E-06		9.43E-06		1.93E-03	1.93E-03	9.52E-08	
TIC	2.08E+04	2.07E+04	1.01E+02		1.01E+02		2.07E+04	2.07E+04	1.02E+00	
UDH2	4.33E+02	4.31E+02	2.11E+00		2.11E+00		4.31E+02	4.31E+02	2.13E-02	
WH6	1.57E+00	1.57E+00	7.66E-03		7.66E-03		1.57E+00	1.57E+00	7.72E-05	
ZH+2	5.01E-01	4.99E-01	2.44E-03		2.44E-03		4.99E-01	4.99E-01	2.46E-05	
ZH+4	2.07E-02	2.06E-02	1.01E-04		1.01E-04		2.06E-02	2.06E-02	1.02E-06	

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Table B-7 Phase 1 LAW Mass Balance for Batch PCL/7 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	9.85E+03	9.85E+01	9.75E+03		9.75E+03		9.92E+01	9.92E-01	9.82E+01	
RADIONUCLIDES (Cl)										
Cesium							3.89E+04	3.89E+02	3.85E+04	
Strontium										
Technetium										
TRU							2.38E+02	2.38E+00	2.35E+02	
CHEMICALS (kg)										
Ag2O										
Al2O3										
Am3							6.54E-02	6.54E-04	6.47E-02	
Am2O3										
As2O5										
B2O3										
B4O										
BeO										
Bi2O3										
CaO										
ClO										
Cr2O3										
CS2O										
ClO										
EU2O3										
FE2O3										
FORMER										
H2O										
DM4T										
K2O										
La2O3										
MgO										
Mn2O										
MO3										
Na2O										
NI2O3										
NF2										
OH-							1.72E-01	1.72E-03	1.70E-01	
P2O5										
PO2										
RU4							1.84E-01	1.84E-03	1.82E-01	
RU2										
SE3										
SiO2										
Sn2										
SO3										
SOLIDS	9.85E+03	9.85E+01	9.75E+03		9.75E+03		9.85E+01	9.85E-01	9.75E+01	
SR+2							2.80E-01	2.80E-03	2.77E-01	
SHO										
Ta2O7										
TiO2										
U3										
W3										
ZnO										
ZrO2										

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Table B-7 Phase 1 LAW Mass Balance for Batch PCL/7 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	8.72E+02	7.47E+05	6.30E+02		6.30E+02	7.47E+05	1.81E+06	6.36E+02	1.20E+03	1.84E+03
Density (g/L)	1.01E+03	1.31E+03	3.32E+03		3.32E+03	1.31E+03	1.00E+03	3.30E+03	1.00E+03	1.80E+03
Total Mass Flow (kg):										
	8.84E+02	9.81E+05	2.09E+03		2.09E+03	9.81E+05	1.81E+06	2.10E+03	1.20E+03	3.30E+03
RADIONUCLIDES (Ci)										
Cesium	1.54E+01	9.16E+02	3.11E+05		3.11E+05	9.16E+02				
Strontium	2.82E-01	5.72E+03			5.72E+03	5.72E+03				
Technetium	9.19E-03	1.83E+02			1.83E+02	9.16E+01		9.29E+01		9.29E+01
TU	4.00E-03	8.11E+01	1.87E+00		1.87E+00	8.11E+01				
CHEMICALS (kg)										
AG+	2.53E-12	5.18E-08				5.18E-08				
AL(CH)4-	2.99E-01	6.06E+03				6.06E+03				
AM#3	1.10E-06	2.23E-02				2.23E-02				
AS+5	1.48E-12	2.99E-08				2.99E-08				
BP#3	7.23E-11	1.47E-06				1.47E-06				
BA#2	2.47E-07	5.00E-03				5.00E-03				
BE#2	3.26E-13	6.62E-09				6.62E-09				
BI#3	1.20E-15	2.44E-11				2.44E-11				
C-14	2.21E-09	4.48E-05				4.48E-05				
CA#2	1.30E-02	2.64E+02				2.64E+02				
CD#2	5.93E-06	1.20E-01				1.20E-01				
CL-	7.76E-02	1.57E+03				1.57E+03				
CL2							1.57E+03			
CO2							1.05E+05			
CO#2	1.97E+00	3.99E+04				3.99E+04				
CR(CH)4-	2.21E-02	4.49E+02				4.49E+02				
CS#	1.78E-04	1.06E-02	3.59E+00		3.59E+00	1.06E-02				
CI#2	4.45E-06	9.03E-02				9.03E-02				
EU-154	5.38E-08	1.09E-03				1.09E-03				
F-	9.11E-03	1.85E+02				1.85E+02				
F2							1.85E+02			
FE#3	3.54E-02	7.18E+02				7.18E+02				
H2O	8.66E+02	6.18E+05				6.18E+05	6.26E+05		1.20E+03	1.20E+03
H#2	5.93E-06	1.20E-01				1.20E-01				
K+	7.12E-02	1.44E+03				1.44E+03				
LA#3	2.63E-06	5.34E-02				5.34E-02				
MA#2	1.23E-05	2.49E-01				2.49E-01				
MA#4	1.18E-02	2.40E+02				2.40E+02				
MO#6	3.37E-05	6.84E-01				6.84E-01				
Na+	5.89E+00	1.20E+05	1.20E+03		1.20E+03	1.20E+05		1.20E+03		1.20E+03
NI#3	1.06E-02	2.16E+02				2.16E+02				
NO2							1.21E+05			
NO2-	1.51E+00	3.06E+04				3.06E+04				
NO3-	5.98E+00	1.21E+05				1.21E+05				
NP#4	5.55E-07	1.13E-02				1.13E-02				
O2							9.51E+05			
OH-	5.09E-01	1.03E+04	8.89E+02		8.89E+02	1.03E+04		8.89E+02		8.89E+02
HM#4	7.80E-03	1.58E+02				1.58E+02				
RO#-3	1.78E-02	3.60E+02				3.60E+02				
RU#4	3.10E-06	6.29E-02				6.29E-02				
SE#6	6.66E-10	1.35E-05				1.35E-05				
SI#4	1.71E-03	3.47E+01				3.47E+01				
SM#4	2.01E-15	4.08E-11				4.08E-11				
SO#-2	4.32E-01	8.77E+03				8.77E+03				
SR#2	2.03E-06	4.11E-02				4.11E-02				
TDA-	6.90E-04	1.39E+01			1.81E-01	8.07E+00				
TI#4	9.50E-08	1.93E-03	1.81E-01		1.81E-01	1.93E-03		9.00E+00		9.00E+00
TCC	1.02E+00	2.07E+04				2.07E+04				
UD#2	2.13E-02	4.31E+02				4.31E+02				
W#6	7.72E-05	1.57E+00				1.57E+00				
ZN#2	2.46E-05	4.99E-01				4.99E-01				
ZR#4	1.02E-06	2.06E-02				2.06E-02				

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Table B-7 Phase 1 LAW Mass Balance for Batch PCL/7 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SLID COMPONENTS										
Total Mass Flow (kg)	9.82E+01	9.92E-01		1.20E+03	1.20E+03	9.92E-01	1.77E+05			
RADIONUCLIDES (Ci)										
Cesium										
Strontium	3.85E+04	3.89E+02				3.89E+02	9.16E+02			
Technetium							6.11E+03			
TRU	2.33E+02	2.38E+00				2.38E+00	9.16E+01			8.12E+01
CHEMICALS (kg)										
AG2O							5.56E-08			
AL2O3							3.25E+03			
AM3	6.47E-02	6.54E-04				6.54E-04				
AM2O3							2.53E-02			
AS2O5							4.59E-06			
B2O3							4.73E-06			
B4O							5.59E-03			
B2O							1.84E-06			
Bi2O3							2.72E-11			
CaO							3.69E+02			
ClO							1.38E-01			
CR2O3							2.84E+02			
CS2O							1.12E-02			
ClO							1.13E-01			
EU2O3							1.26E-03			
FE2O3							1.03E+03			
FORMER										
H2O							1.30E-01			
DMAT				1.20E+03	1.20E+03					
K2O							1.74E+03			
LA2O3							6.26E-02			
M2O							4.14E-01			
MN2							3.80E+02			
MO3							1.03E+00			
Na2O							1.61E+05			
Ni2O3							3.04E+02			
NFO2							1.28E-02			
OH-										
P2O5	1.70E-01	1.72E-03				1.72E-03	2.69E+02			
PO2							1.83E+02			
PH4	1.82E-01	1.84E-03				1.84E-03				
PI2							7.34E-02			
SE03							2.17E-05			
SiO2							7.43E+01			
SiO2							5.17E-11			
SO3							7.31E+03			
SOLIDS	9.75E+01	9.85E-01				9.85E-01	9.85E-01			
SR+2	2.77E-01	2.80E-03				2.80E-03				
SRO							5.17E-02			
TC2O7							8.44E+00			
TI02							3.21E-03			
UO3							4.57E+02			
VO3							1.97E+00			
ZNO							6.21E-01			
ZrO2							2.79E-02			

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Table B-7 Phase 1 LAW Mass Balance for Batch PCL/7 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	1.81E+06				1.18E+06	6.26E+05	6.27E+02	6.27E+02	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	1.81E+06				1.18E+06	6.26E+05	2.09E+03	2.09E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
BH+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	1.57E+03				1.57E+03				
CO2	1.05E+05				1.05E+05				
CO3-2									
CR(OH)4-									
CS+									
ClH2									
EU-154									
F-									
F2	1.83E+02				1.85E+02				
FE+3									
H2O	6.26E+05					6.26E+05			
HP+2									
IS-									
LA+3									
MG+2									
MN+4									
MD+6									
NA+							1.20E+03	1.20E+03	
NI+3									
NO2	1.21E+05				1.21E+05				
NO2-									
NO3-									
NO4-									
O2	9.51E+05				9.51E+05				
OH-									
OH4							8.89E+02	8.89E+02	1.00E+06
FO4-3									
HU+4									
SE+6									
SI+4									
SR+4									
SO4-2									
SR+2									
TOD-									
TI+4									
TOC									
UO2+2									
W+6									
ZN+2									
ZR+4									

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Table B-7 Phase 1 LAW Mass Balance for Batch PCL/7 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		1.77E+05	7.78E+05	9.54E+05					
RADIONUCLIDES (Ci)									
Cesium		9.16E+02		9.16E+02					
Strontium		6.11E+03		6.11E+03					
Technetium		9.16E+01		9.16E+01					
TRU		8.12E+01		8.12E+01					
CHEMICALS (kg)									
AC2O		5.56E-08		5.56E-08					
AL2O3		3.25E+03		3.25E+03					
AM#3									
AM#3		2.53E-02		2.53E-02					
AS2O5		4.59E-08		4.59E-08					
EGO3		4.73E-06		4.73E-06					
BAO		5.59E-03		5.59E-03					
BE2		1.84E-08		1.84E-08					
EU2O3		2.72E-11		2.72E-11					
CAO		3.69E+02		3.69E+02					
ClO		1.38E-01		1.38E-01					
CR2O3		2.84E+02		2.84E+02					
CS2O		1.12E-02		1.12E-02					
ClO		1.13E-01		1.13E-01					
EU2O3		1.26E-03		1.26E-03					
FE2O3		1.03E+03		1.03E+03					
FORMER			7.78E+05	7.78E+05					
H2O		1.30E-01		1.30E-01					
IM#41									
IG2		1.74E+03		1.74E+03					
LA2O3		6.26E-02		6.26E-02					
MD		4.14E-01		4.14E-01					
MND2		3.80E+02		3.80E+02					
MO3		1.03E+00		1.03E+00					
NA2O		1.61E+05		1.61E+05					
NL2O3		3.04E+02		3.04E+02					
NFO2		1.28E-02		1.28E-02					
OH-									
P2O5		2.69E+02		2.69E+02					
PE2O		1.83E+02		1.83E+02					
PH4									
PU2		7.34E-02		7.34E-02					
SE2O3		2.17E-05		2.17E-05					
SiO2		7.43E+01		7.43E+01					
SN2		5.17E-11		5.17E-11					
SO3		7.31E+03		7.31E+03					
SULFIDS		9.85E-01		9.85E-01					
SR#2									
SrO		5.17E-02		5.17E-02					
TC2O7		8.44E+00		8.44E+00					
TiO2		3.21E-03		3.21E-03					
UD3		4.57E+02		4.57E+02					
W2O3		1.97E+00		1.97E+00					
ZNO		6.21E-01		6.21E-01					
ZrO2		2.79E-02		2.79E-02					

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Table B-8 Phase 1 IAW Mass Balance for Batch PCL/8 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	1.52E+06	1.52E+06	7.21E+03	1.69E+05	1.76E+05		1.52E+06	1.52E+06	7.27E+01	1.70E+03
Density (g/L)	1.32E+03	1.32E+03	1.32E+03	1.00E+03	1.01E+03		1.32E+03	1.32E+03	1.32E+03	1.00E+03
Total Mass Flow (kg)	2.00E+06	2.00E+06	9.49E+03	1.69E+05	1.79E+05		2.00E+06	2.00E+06	9.57E+01	1.70E+03
RADIONUCLIDES (Ci)										
Cesium	4.09E+05	4.07E+05	1.94E+03		1.94E+03		4.07E+05	4.07E+05	1.95E+01	
Strontium	1.01E+05	1.01E+05	4.78E+02		4.78E+02		1.19E+04	1.19E+04	5.71E-01	
Technetium	3.64E+02	3.62E+02	1.72E+00		1.72E+00		3.62E+02	3.62E+02	1.74E-02	
IU	7.23E+02	7.19E+02	3.42E+00		3.42E+00		1.70E+02	1.70E+02	8.14E-03	
CHEMICALS (kg)										
AGP	1.32E-08	1.32E-08	6.26E-11		6.26E-11		1.32E-08	1.32E-08	6.31E-13	
AL(OH)4-	6.96E+03	6.92E+03	3.29E+01		3.29E+01		6.92E+03	6.92E+03	3.32E-01	
AMP3	2.00E-01	1.99E-01	9.45E-04		9.45E-04		4.69E-02	4.69E-02	2.25E-06	
ASH5	7.64E-09	7.60E-09	3.62E-11		3.62E-11		7.60E-09	7.60E-09	3.65E-13	
BH3	3.74E-07	3.72E-07	1.77E-09		1.77E-09		3.72E-07	3.72E-07	1.79E-11	
BH42	3.36E-03	3.36E-03	1.60E-05		1.60E-05		3.36E-03	3.36E-03	1.61E-07	
BEH2	1.69E-09	1.68E-09	7.98E-12		7.98E-12		1.68E-09	1.68E-09	8.04E-14	
BIH3	6.23E-12	6.20E-12	2.95E-14		2.95E-14		6.20E-12	6.20E-12	2.97E-16	
C-14	2.95E-05	2.93E-05	1.40E-07		1.40E-07		2.93E-05	2.93E-05	1.41E-09	
CAH2	6.01E+02	5.98E+02	2.84E+00		2.84E+00		5.98E+02	5.98E+02	2.87E-02	
CDH2	5.18E-02	5.15E-02	2.45E-04		2.45E-04		5.15E-02	5.15E-02	2.47E-06	
CL-	3.42E+03	3.41E+03	1.62E+01		1.62E+01		3.41E+03	3.41E+03	1.63E-01	
CL2										
CO2										
CO3-2										
CR(OH)4-	8.45E+04	8.41E+04	4.00E+02		4.00E+02		8.41E+04	8.41E+04	4.03E+00	
CSH3	6.01E+02	5.99E+02	2.83E+00		2.83E+00		5.99E+02	5.99E+02	2.87E-02	
CSH	4.73E+00	4.70E+00	2.24E-02		2.24E-02		4.70E+00	4.70E+00	2.26E-04	
CH2	3.88E-02	3.86E-02	1.84E-04		1.84E-04		3.86E-02	3.86E-02	1.85E-06	
EU-154	7.37E-04	7.34E-04	3.49E-06		3.49E-06		7.34E-04	7.34E-04	3.52E-08	
F-	1.24E+02	1.23E+02	5.85E-01		5.85E-01		1.23E+02	1.23E+02	5.90E-03	
F2										
FEH3	1.63E+03	1.63E+03	7.73E+00		7.73E+00		1.63E+03	1.63E+03	7.79E-02	
HD2	1.24E+06	1.24E+06	5.89E+03	1.69E+05	1.72E+05		1.24E+06	1.24E+06	5.94E+01	1.70E+03
HM2	5.18E-02	5.15E-02	2.43E-04		2.43E-04		5.15E-02	5.15E-02	2.47E-06	
HP	2.58E+03	2.56E+03	1.22E+01		1.22E+01		2.56E+03	2.56E+03	1.23E-01	
IAlH3	3.61E-02	3.59E-02	1.71E-04		1.71E-04		3.59E-02	3.59E-02	1.72E-06	
MDH2	1.08E-01	1.08E-01	5.12E-04		5.12E-04		1.08E-01	1.08E-01	5.16E-06	
MNH4	5.46E+02	5.44E+02	2.59E+00		2.59E+00		5.44E+02	5.44E+02	2.61E-02	
NDH6	2.93E-01	2.92E-01	1.39E-03		1.39E-03		2.92E-01	2.92E-01	1.40E-05	
NAH	2.51E+05	2.50E+05	1.19E+03		1.19E+03		2.50E+05	2.50E+05	1.20E+01	
NIH3	4.91E+02	4.88E+02	2.32E+00		2.32E+00		4.88E+02	4.88E+02	2.34E-02	
NO2										
NO2-	5.82E+04	5.80E+04	2.76E+02		2.76E+02		5.80E+04	5.80E+04	2.78E+00	
NO3-	2.64E+05	2.62E+05	1.23E+03		1.23E+03		2.62E+05	2.62E+05	1.26E+01	
NOH4	7.55E-03	7.52E-03	3.58E-05		3.58E-05		7.52E-03	7.52E-03	3.60E-07	
O2										
OH-	2.05E+04	2.04E+04	9.70E+01		9.70E+01		2.04E+04	2.04E+04	9.77E-01	
FBH4	3.60E+02	3.59E+02	1.71E+00		1.71E+00		3.59E+02	3.59E+02	1.72E-02	
FO4-3	6.48E+02	6.45E+02	3.07E+00		3.07E+00		6.45E+02	6.45E+02	3.09E-02	
FUH4	5.26E-01	5.23E-01	2.49E-03		2.49E-03		1.24E-01	1.24E-01	5.94E-06	
SEH6	4.59E-06	4.52E-06	2.15E-08		2.15E-08		4.52E-06	4.52E-06	2.17E-10	
SIH4	2.30E+01	2.29E+01	1.09E-01		1.09E-01		2.29E+01	2.29E+01	1.10E-03	
SNH4	1.04E-11	1.03E-11	4.91E-14		4.91E-14		1.03E-11	1.03E-11	4.95E-16	
SO4-2	1.64E+04	1.63E+04	7.77E+01		7.77E+01		1.63E+04	1.63E+04	7.84E-01	
SRH+2	7.27E-01	7.23E-01	3.44E-03		3.44E-03		8.56E-02	8.56E-02	4.11E-06	
TCO4-	2.53E+01	2.51E+01	1.67E-01		1.67E-01		3.51E+01	3.51E+01	1.66E-03	
TIH4	6.50E-04	6.47E-04	3.08E-06		3.08E-06		6.47E-04	6.47E-04	3.10E-08	
TICL	4.69E+04	4.67E+04	2.22E+02		2.22E+02		4.67E+04	4.67E+04	2.24E+00	
UD2+2	6.60E+02	6.57E+02	3.13E+00		3.13E+00		6.57E+02	6.57E+02	3.15E-02	
WH6	6.73E-01	6.70E-01	3.19E-03		3.19E-03		6.70E-01	6.70E-01	3.21E-05	
ZNH2	2.05E-01	2.04E-01	9.70E-04		9.70E-04		2.04E-01	2.04E-01	9.77E-06	
ZRH4	6.94E-03	6.91E-03	3.29E-05		3.29E-05		6.91E-03	6.91E-03	3.31E-07	

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Table B-8 Phase 1 LAW Mass Balance for Batch FCL/8 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	2.00E+04	2.00E+02	1.98E+04		1.98E+04		2.02E+02	2.02E+00	2.00E+02	
RADIONUCLIDES (Ci)										
Cesium										
Strontium							8.86E+04	8.86E+02	8.77E+04	
Technetium										
TU							5.50E+02	5.50E+00	5.44E+02	
CHEMICALS (kg)										
AC2O										
AL2O3										
AM+3							1.52E-01	1.52E-03	1.50E-01	
AM2O3										
AS2O5										
EGO3										
EAO										
EEO										
ELZG3										
CAO										
CIO										
CR2O3										
CS2O										
CUD										
EUGO3										
FE2O3										
FORMER										
H2O										
DMFAT										
K2O										
LA2O3										
MGO										
MNO2										
MCO3										
NA2O										
NIL2O3										
NEO2										
OH-							3.87E-01	3.87E-03	3.83E-01	
PO25										
PBO2										
FU+4							3.99E-01	3.99E-03	3.95E-01	
FUC2										
SBO3										
SIO2										
SN22										
SO3										
SULFUR	2.00E+04	2.00E+02	1.98E+04		1.98E+04		2.00E+02	2.00E+00	1.98E+02	
SR+2							6.38E-01	6.38E-03	6.31E-01	
SRO										
TIC2O7										
TIO2										
UD3										
WCO										
ZNO										
ZR2O2										

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Table B-8 Phase 1 LAW Mass Balance for Batch PCL/8 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	1.78E+03	1.52E+06	1.32E+03		1.32E+03	1.52E+06	2.63E+06	1.33E+03	2.51E+03	3.84E+03
Density (g/L)	1.01E+03	1.32E+03	3.33E+03		3.33E+03	1.32E+03	1.00E+03	3.31E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)	1.80E+03	2.00E+06	4.38E+03		4.38E+03	2.00E+06	2.63E+06	4.39E+03	2.51E+03	6.90E+03
RADIONUCLIDES (Ci)										
Cesium	1.95E+01	1.92E+03	4.05E+05		4.05E+05	1.92E+03				
Strontium	5.77E-01	1.19E+04				1.19E+04				
Technetium	1.74E-02	3.59E+02			3.64E+00	1.92E+02		1.67E+02		1.92E+02
IU	8.14E-03	1.70E+02	3.64E+00			1.70E+02				1.67E+02
CHEMICALS (kg)										
AGP	6.31E-13	1.32E-08				1.32E-08				
AL(OH)4-	3.32E-01	6.92E+03				6.92E+03				
AM#3	2.22E-06	4.69E-02				4.69E-02				
AS#5	3.63E-13	7.50E-09				7.60E-09				
B#3	1.79E-11	3.72E-07				3.72E-07				
BA#2	1.61E-07	3.34E-03				3.34E-03				
BE#2	8.04E-14	1.64E-09				1.68E-09				
BI#3	2.97E-16	6.20E-12				6.20E-12				
C-14	1.41E-09	2.93E-05				2.93E-05				
CA#2	2.87E-02	5.98E+02				5.98E+02				
CD#2	2.47E-06	5.15E-02				5.15E-02				
CL-	1.63E-01	3.41E+03				3.41E+03				
CL2							3.41E+03			
CO2							2.33E+05			
CO3-2	4.03E+00	8.41E+04				8.41E+04				
CR(OH)4-	2.87E-02	5.99E+02				5.99E+02				
CSH	2.26E-04	2.21E-02	4.68E+00		4.68E+00	2.21E-02				
CU#2	1.85E-06	3.86E-02				3.86E-02				
EJ-154	3.52E-08	7.34E-04				7.34E-04				
F-	5.90E-03	1.23E+02				1.23E+02				
F2							1.23E+02			
FE#3	7.79E-02	1.63E+03				1.63E+03				
H2O	1.76E+03	1.24E+06				1.24E+06	1.25E+06		2.51E+03	2.51E+03
H#2	2.47E-06	5.13E-02				5.13E-02				
H+	1.22E-01	2.56E+03				2.56E+03				
IA#3	1.72E-06	3.59E-02				3.59E-02				
MD#2	5.16E-06	1.08E-01				1.08E-01				
M#4	2.61E-02	5.43E+02				5.43E+02				
ND#6	1.40E-05	2.92E-01				2.92E-01				
NA+	1.20E+01	2.50E+05	2.51E+03		2.51E+03	2.50E+05		2.51E+03		2.51E+03
NI#3	2.34E-02	4.88E+02				4.88E+02				
NO2							2.53E+05			
NO2-	2.78E+00	5.80E+04				5.80E+04				
NO3-	1.26E+01	2.62E+05				2.62E+05				
NO#4	3.60E-07	7.52E-03				7.52E-03				
O2							8.90E+05			
OH-	9.77E-01	2.04E+04	1.86E+03		1.86E+03	2.04E+04		1.86E+03		1.86E+03
OH#4	1.72E-02	3.59E+02				3.59E+02				
FO4-3	3.09E-02	6.45E+02				6.45E+02				
FU#4	5.94E-06	1.24E-01				1.24E-01				
SE#6	2.17E-10	4.52E-06				4.52E-06				
SI#4	1.10E-03	2.29E+01				2.29E+01				
SH#4	4.95E-16	1.03E-11				1.03E-11				
SD#2	7.84E-01	1.63E+04				1.63E+04				
SH#2	4.11E-06	8.54E-02				8.54E-02				
TDO4-	1.68E-03	3.47E+01	3.53E-01		3.53E-01	1.86E+01		1.62E+01		1.62E+01
TI#4	3.10E-08	6.47E-04				6.47E-04				
TCC	2.24E+00	4.67E+04				4.67E+04				
UO2#2	3.15E-02	6.57E+02				6.57E+02				
WH6	3.21E-05	6.70E-01				6.70E-01				
ZH#2	9.77E-06	2.04E-01				2.04E-01				
ZH#4	3.31E-07	6.91E-03				6.91E-03				

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Table B-8 Phase 1 LAW Mass Balance for Batch PCL/8 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	2.00E+02	2.02E+00		2.51E+03	2.51E+03	2.02E+00	3.65E+05			
RADIONUCLIDES (Ci)										
Cesium							1.92E+03			
Strontium	8.77E+04	8.86E+02				8.86E+02	1.28E+04			
Technetium							1.92E+02			
TRU	5.44E+02	5.50E+00				5.50E+00	1.70E+02			
CHEMICALS (kg)										
AC2O3							1.41E-08			
AL2O3							3.71E+03			
AM43	1.50E-01	1.52E-03				1.52E-03				
AM2O3							5.32E-02			
AS2O5							1.17E-08			
B2O3							1.20E-06			
B4O							3.75E-03			
B2O							4.65E-09			
BL2O3							6.91E-12			
CaO							8.36E+02			
ClO							5.88E-02			
CR2O3							3.79E+02			
CS2O							2.34E-02			
CUO							4.83E-02			
EU2O3							8.49E-04			
FE2O3							2.32E+03			
FORMER							5.56E-02			
H2O										
HM2AT				2.51E+03	2.51E+03					
K2O							3.09E+03			
LA2O3							4.22E-02			
MCO							1.79E-01			
MNO2							8.60E+02			
MCO3							4.37E-01			
NA2O							3.37E+05			
NIL2O3							6.88E+02			
NEO2							8.53E-03			
OH-	3.63E-01	3.87E-03				3.87E-03				
FeO5							4.82E+02			
FeO2							4.14E+02			
HU4	3.95E-01	3.99E-03				3.99E-03				
FeO2							1.45E-01			
SeO3							7.27E-06			
SiO2							4.89E+01			
SnO2							1.31E-11			
SO3							1.36E+04			
SOLIDS	1.98E+02	2.00E+00				2.00E+00	2.00E+00			
SR+2	6.31E-01	6.39E-03				6.39E-03				
SrO							1.08E-01			
TC2O7							1.77E+01			
TiO2							1.08E-03			
UO3							6.96E+02			
WCO							8.45E-01			
ZNO							2.54E-01			
ZrO2							9.33E-03			

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Table B-8 Phase 1 LAW Mass Balance for Batch PCL/8 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	2.63E+06				1.38E+06	1.23E+06	1.31E+03	1.31E+03	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	2.63E+06				1.38E+06	1.23E+06	4.38E+03	4.38E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AD+									
AL(OH)4-									
As+3									
As+5									
B+3									
Be+2									
Bi+3									
C-14									
Ca+2									
CD+2									
CL-									
CL2	3.41E+03				3.41E+03				
CO2	2.33E+05				2.33E+05				
CO3-2									
CR(OH)4-									
CS+									
Cl+2									
EJ-154									
F-									
F2	1.23E+02				1.23E+02				
Fe+3									
H2O	1.25E+06					1.25E+06			
Hg+2									
K+									
LA+3									
MD+2									
MN+4									
ND+6									
Na+							2.51E+03	2.51E+03	
NI+3									
NO2	2.53E+05				2.53E+05				
NO2-									
NO3-									
NE+4									
O2	8.90E+05				8.90E+05				1.00E+06
OH-							1.86E+03	1.86E+03	
PH+4									
PO4-3									
PU+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TCD+4-									
TI+4									
TCC									
UDC+2									
WH+6									
ZH+2									
Zr+4									

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Table B-8 Phase 1 LAW Mass Balance for Batch PCL/8 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		3.65E+05	1.63E+06	2.00E+06					
RADIONUCLIDES (Ci)									
Cesium		1.92E+03		1.92E+03					
Strontium		1.28E+04		1.28E+04					
Technetium		1.92E+02		1.92E+02					
TU1		1.70E+02		1.70E+02					
CHEMICALS (kg)									
AC2O		1.41E-08		1.41E-08					
AL2O3		3.71E+03		3.71E+03					
AM+3									
AM2O3		5.32E-02		5.32E-02					
AS2O5		1.17E-08		1.17E-08					
B2O3		1.20E-06		1.20E-06					
B4O		3.73E-03		3.73E-03					
B4O7		4.63E-09		4.63E-09					
BL2O3		6.91E-12		6.91E-12					
CaO		8.36E+02		8.36E+02					
CaO		5.88E-02		5.88E-02					
CR2O3		3.79E+02		3.79E+02					
CS2O		2.34E-02		2.34E-02					
CUO		4.83E-02		4.83E-02					
EU2O3		8.49E-04		8.49E-04					
FE2O3		2.32E+03		2.32E+03					
FORMER			1.63E+06						
H2O		5.56E-02		5.56E-02					
IMPHAT									
K2O		3.09E+03		3.09E+03					
LA2O3		4.22E-02		4.22E-02					
MO3		1.78E-01		1.78E-01					
MNO2		8.60E+02		8.60E+02					
MCO3		4.37E-01		4.37E-01					
NA2O		3.37E+05		3.37E+05					
NIL2O3		6.88E+02		6.88E+02					
NEO2		8.53E-03		8.53E-03					
OH-									
PO25		4.82E+02		4.82E+02					
PKO2		4.14E+02		4.14E+02					
RU+4									
RUO2		1.45E-01		1.45E-01					
SEO3		7.27E-06		7.27E-06					
SI02		4.89E+01		4.89E+01					
SN02		1.31E-11		1.31E-11					
SO3		1.36E+04		1.36E+04					
SOLIDS		2.00E+00		2.00E+00					
SR+2									
SRO		1.08E-01		1.08E-01					
TCCO7		1.77E+01		1.77E+01					
TIO2		1.08E-03		1.08E-03					
UC3		6.96E+02		6.96E+02					
UC3		8.45E-01		8.45E-01					
ZNO		2.54E-01		2.54E-01					
ZNO2		9.33E-03		9.33E-03					

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Table B-9 Phase 1 LAW Mass Balance for Batch PCL/9 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	2.99E+06	2.98E+06	1.41E+04	3.31E+05	3.45E+05		2.98E+06	2.98E+06	1.41E+02	3.32E+03
Density (g/L)	1.31E+03	1.31E+03	1.31E+03	1.00E+03	1.01E+03		1.31E+03	1.31E+03	1.31E+03	1.00E+03
Total Mass Flow (kg)	3.92E+06	3.90E+06	1.84E+04	3.31E+05	3.50E+05		3.90E+06	3.90E+06	1.85E+02	3.32E+03
RADIONUCLIDES (Ci)										
Cesium	4.98E+05	4.95E+05	2.34E+03		2.34E+03		4.95E+05	4.95E+05	2.35E+01	
Strontium	1.50E+05	1.49E+05	7.07E+02		7.07E+02		2.39E+04	2.39E+04	1.14E+00	
Technetium	5.84E+02	5.82E+02	2.78E+00		2.75E+00		5.82E+02	5.82E+02	2.76E+02	
IU	3.23E+02	3.22E+02	1.52E+00		1.52E+00		3.22E+02	3.22E+02	1.53E+02	
CHEMICALS (kg)										
AGP	1.24E-09	1.24E-09	5.86E-12		5.86E-12		1.24E-09	1.24E-09	5.87E-14	
AL(OH)4-	9.16E+04	9.12E+04	4.31E+02		4.31E+02		9.12E+04	9.12E+04	4.32E+00	
AM+3	5.56E-02	5.54E-02	2.62E-04		2.62E-04		5.54E-02	5.54E-02	2.63E-06	
AS+5	7.23E-10	7.18E-10	3.40E-12		3.40E-12		7.18E-10	7.18E-10	3.41E-14	
BA+3	3.53E-08	3.52E-08	1.65E-10		1.65E-10		3.52E-08	3.52E-08	1.67E-12	
BA+2	3.83E-04	3.81E-04	1.80E-06		1.80E-06		3.81E-04	3.81E-04	1.81E-08	
BE+2	1.59E-10	1.58E-10	7.48E-13		7.48E-13		1.58E-10	1.58E-10	7.51E-15	
BI+3	5.88E-13	5.86E-13	2.77E-15		2.77E-15		5.86E-13	5.86E-13	2.78E-17	
C-14	7.16E-03	7.13E-03	3.37E-05		3.37E-05		7.13E-03	7.13E-03	3.38E-07	
CA+2	8.41E+02	8.37E+02	3.96E+00		3.96E+00		8.37E+02	8.37E+02	3.97E+02	
CD+2	5.52E-03	5.50E-03	2.60E-05		2.60E-05		5.50E-03	5.50E-03	2.61E-07	
CL-	7.21E+03	7.17E+03	3.39E+01		3.39E+01		7.17E+03	7.17E+03	3.40E+01	
CL2										
CO2										
CO3-2	1.27E+05	1.26E+05	5.98E+02		5.98E+02		1.26E+05	1.26E+05	6.00E+00	
CR(OH)4-	1.22E+03	1.21E+03	5.73E+00		5.73E+00		1.21E+03	1.21E+03	5.73E+02	
CS+	5.75E+00	5.72E+00	2.70E-02		2.70E-02		5.72E+00	5.72E+00	2.71E-04	
ClH2	4.14E-03	4.12E-03	1.95E-05		1.95E-05		4.12E-03	4.12E-03	1.95E-07	
EU-154	5.34E-03	5.31E-03	2.51E-05		2.51E-05		5.31E-03	5.31E-03	2.52E-07	
F-	3.64E+03	3.64E+03	1.72E+01		1.72E+01		3.64E+03	3.64E+03	1.73E+01	
F2										
FE+3	1.98E+02	1.97E+02	9.31E-01	3.31E+05	9.31E-01		1.97E+02	1.97E+02	9.34E-03	
H2O	2.51E+06	2.49E+06	1.18E+04		2.49E+05		2.49E+06	2.49E+06	1.18E+02	3.32E+03
HG+2	5.52E-03	5.50E-03	2.60E-05		2.60E-05		5.50E-03	5.50E-03	2.61E-07	
K+	7.12E+03	7.09E+03	3.33E+01		3.33E+01		7.09E+03	7.09E+03	3.36E+01	
LA+3	4.08E-03	4.06E-03	1.92E-05		1.92E-05		4.06E-03	4.06E-03	1.93E-07	
MS+2	1.16E-02	1.15E-02	5.43E-05		5.43E-05		1.15E-02	1.15E-02	5.47E-07	
MN+4	6.61E+01	6.58E+01	3.11E-01		3.11E-01		6.58E+01	6.58E+01	3.12E-03	
MO+6	3.12E-02	3.10E-02	1.47E-04		1.47E-04		3.10E-02	3.10E-02	1.47E-06	
NA+	4.95E+05	4.93E+05	2.33E+03		2.33E+03		4.93E+05	4.93E+05	2.34E+01	
NI+3	6.73E+02	6.70E+02	3.17E+00		3.17E+00		6.70E+02	6.70E+02	3.18E+02	
NO2										
NO2-	1.53E+05	1.52E+05	7.20E+02		7.20E+02		1.52E+05	1.52E+05	7.22E+00	
NO3-	4.17E+05	4.15E+05	1.96E+03		1.96E+03		4.15E+05	4.15E+05	1.97E+01	
NE+4	8.54E-04	8.50E-04	4.02E-06		4.02E-06		8.50E-04	8.50E-04	4.03E-08	
O2										
OH-	2.12E+04	2.11E+04	9.96E+01		9.96E+01		2.11E+04	2.11E+04	9.99E+01	
OH+4	4.36E+01	4.34E+01	2.05E-01		2.05E-01		4.34E+01	4.34E+01	2.06E+03	
FO4-3	8.64E+03	8.60E+03	4.07E+01		4.07E+01		8.60E+03	8.60E+03	4.08E+01	
FO4+4	1.83E+00	1.82E+00	8.61E-03		8.61E-03		1.82E+00	1.82E+00	8.64E-05	
SE+6	4.63E-07	4.61E-07	2.18E-09		2.18E-09		4.61E-07	4.61E-07	2.19E-11	
SI+4	2.59E+00	2.58E+00	1.22E-02		1.22E-02		2.58E+00	2.58E+00	1.22E-04	
SN+4	9.85E-13	9.80E-13	4.64E-15		4.64E-15		9.80E-13	9.80E-13	4.65E-17	
SO4-2	2.70E+04	2.69E+04	1.27E+02		1.27E+02		2.69E+04	2.69E+04	1.28E+00	
SR+2	1.08E+00	1.08E+00	5.08E-03		5.08E-03		1.07E+01	1.07E+01	8.16E-06	
TIO4-	5.64E+01	5.63E+01	2.64E-01		2.64E-01		5.63E+01	5.63E+01	2.67E+03	
TC+4	6.61E-05	6.58E-05	3.11E-07		3.11E-07		6.58E-05	6.58E-05	3.12E-09	
TCC	5.15E+04	5.13E+04	2.42E+02		2.42E+02		5.13E+04	5.13E+04	2.43E+00	
UDC+2	7.88E+01	7.84E+01	3.71E-01		3.71E-01		7.84E+01	7.84E+01	3.72E+03	
WH+6	7.18E-02	7.15E-02	3.38E-04		3.38E-04		7.15E-02	7.15E-02	3.39E-06	
ZN+2	2.17E-02	2.16E-02	1.02E-04		1.02E-04		2.16E-02	2.16E-02	1.02E-06	
ZR+4	7.06E-04	7.03E-04	3.32E-06		3.32E-06		7.03E-04	7.03E-04	3.33E-08	

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Table B-9 Phase 1 LAW Mass Balance for Batch PCL/9 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.92E+04	3.92E+02	3.88E+04		3.88E+04		3.94E+02	3.94E+00	3.90E+02	
RADIONUCLIDES (Cl)										
Cesium										
Strontium							1.26E+05	1.26E+03	1.24E+05	
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B4O7										
Bi2O3										
CaO										
Cl2										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
H2O										
IMMAT										
K2O										
LA2O3										
MO										
MO2										
MO3										
NA2O										
NI2O3										
NI2O2										
OH-										
PO5							3.41E-01	3.41E-03	3.38E-01	
PO2										
HU2										
SE2O3										
SI2O2										
SN2O2										
SO3										
SOLIDS	3.92E+04	3.92E+02	3.88E+04		3.88E+04		3.92E+02	3.92E+00	3.88E+02	
SR+2							9.03E-01	9.03E-03	8.94E-01	
SRO										
TC2O7										
TiO2										
UO3										
WO3										
ZNO										
ZRO2										

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Table B-9 Phase 1 LAW Mass Balance for Batch PCL/9 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	3.46E+03	2.98E+06	2.59E+03		2.59E+03	2.98E+06	4.15E+06	2.60E+03	4.95E+03	7.53E+03
Density (g/L)	1.01E+03	1.31E+03	3.33E+03		3.33E+03	1.31E+03	1.00E+03	3.32E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)	3.51E+03	3.90E+06	8.62E+03		8.62E+03	3.90E+06	4.15E+06	8.63E+03	4.95E+03	1.36E+04
RADIONUCLIDES (Ci)										
Cesium	2.35E+01	3.78E+03	4.91E+05		4.91E+05	3.78E+03				
Strontium	1.14E+00	2.39E+04				2.39E+04				
Technetium	2.76E-02	5.76E+02	5.64E+00		5.64E+00	3.78E+02		1.98E+02		1.98E+02
IU1	1.53E-02	3.22E+02				3.22E+02				
CHEMICALS (kg)										
AG+	5.87E-14	1.24E-09				1.24E-09				
AL(OH)4-	4.32E+00	9.12E+04				9.12E+04				
AP+3	2.63E-06	5.54E-02				5.54E-02				
AS+5	3.41E-14	7.18E-10				7.18E-10				
B+3	1.67E-12	3.32E-08				3.32E-08				
BA+2	1.81E-08	3.81E-04				3.81E-04				
BE+2	7.51E-15	1.58E-10				1.58E-10				
BI+3	2.78E-17	5.86E-13				5.86E-13				
C-14	3.38E-07	7.13E-03				7.13E-03				
CA+2	3.97E-02	8.37E+02				8.37E+02				
CD+2	2.61E-07	5.50E-03				5.50E-03				
CL-	3.40E-01	7.17E+03				7.17E+03				
CL2							7.17E+03			
CO2							2.81E+05			
CO3-2	6.00E+00	1.26E+05				1.26E+05				
CR(OH)4-	5.73E-02	1.21E+03				1.21E+03				
CS+	2.71E-04	4.36E-02	5.68E+00		5.68E+00	4.36E-02				
ClH2	1.95E-07	4.12E-03				4.12E-03				
EU-154	2.52E-07	5.31E-03				5.31E-03				
F-	1.73E-01	3.64E+03				3.64E+03				
F2							3.64E+03			
FE+3	9.34E-03	1.97E+02				1.97E+02				
H2O	3.44E+03	2.49E+06				2.49E+06	2.54E+06		4.95E+03	4.95E+03
H3+2	2.61E-07	5.50E-03				5.50E-03				
K+	3.36E-01	7.09E+03				7.09E+03				
LA+3	1.93E-07	4.06E-03				4.06E-03				
MG+2	5.47E-07	1.15E-02				1.15E-02				
MN+4	3.12E-03	6.58E+01				6.58E+01				
MO+6	1.47E-06	3.10E-02				3.10E-02				
NA+	2.34E+01	4.93E+05	4.93E+03		4.93E+03	4.93E+05		4.93E+03		4.93E+03
NI+3	3.18E-02	6.70E+02				6.70E+02				
NO2							4.60E+05			
NO2-	7.22E+00	1.52E+05				1.52E+05				
NO3-	1.97E+01	4.13E+05				4.13E+05				
NO3H4	4.03E-08	8.50E-04				8.50E-04				
O2							8.50E+05			
OH-	9.99E-01	2.11E+04	3.66E+03		3.66E+03	2.11E+04		3.66E+03		3.66E+03
OH+4	2.06E-03	4.34E+01				4.34E+01				
FO4-3	4.08E-01	8.60E+03				8.60E+03				
FU+4	8.64E-05	1.82E+00				1.82E+00				
SE+6	2.19E-11	4.61E-07				4.61E-07				
SI+4	1.22E-04	2.58E+00				2.58E+00				
SN+4	4.65E-17	9.80E-13				9.80E-13				
SO4-2	1.28E+00	2.69E+04				2.69E+04				
SR+2	8.16E-06	1.72E-01				1.72E-01				
TU+4-	2.67E-03	5.58E+01				5.58E+01		1.92E+01		1.92E+01
TI+4	3.12E-09	6.58E-05	5.66E-01		5.66E-01	6.58E-05				
TO2	2.43E+00	5.13E+04				5.13E+04				
UD2+2	3.72E-03	7.84E+01				7.84E+01				
W+6	3.39E-06	7.15E-02				7.15E-02				
ZN+2	1.02E-06	2.16E-02				2.16E-02				
ZR+4	3.33E-08	7.03E-04				7.03E-04				

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Table B-9 Phase 1 LAW Mass Balance for Batch PCL/9 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	3.90E+02	3.94E+00		4.95E+03	4.95E+03	3.94E+00	7.54E+05			
RADIONUCLIDES (Cl.)										
Cesium							3.78E+03			
Strontium	1.24E+05	1.26E+03				1.26E+03	2.52E+04			
Technetium							3.78E+02			
TU							3.20E+02			
CHEMICALS (kg)										
AG2O							1.33E-09			
AL2O3							4.89E+04			
AM2O3							6.09E-02			
AS2O3							1.10E-09			
B2O3							1.13E-07			
B4O							4.23E-04			
B4O							4.39E-10			
BI2O3							6.33E-13			
CaO							1.17E+03			
CO							6.28E-03			
CR2O3							7.68E+02			
CS2O							4.62E-02			
CUO							5.16E-03			
EU2O3							6.15E-03			
FE2O3							2.82E+02			
FURMER										
HEO							5.93E-03			
DMF				4.95E+03	4.95E+03					
K2O							8.54E+03			
LA2O3							4.76E-03			
MO							1.91E-02			
MNO2							1.04E+02			
MCO3							4.66E-02			
NA2O							6.64E+05			
NI2O3							9.44E+02			
NEO2							9.64E-04			
CH-	3.38E-01	3.41E-03				3.41E-03				
PCO5							6.43E+03			
PBO2							5.01E+01			
PUO2							2.06E+00			
SBO3							7.41E-07			
STO2							5.52E+00			
SNO2							1.25E-12			
SO3							2.24E+04			
SOLIDS	3.88E+02	3.92E+00				3.92E+00	3.92E+00			
SR+2	8.94E-01	9.03E-03				9.03E-03				
SRO							2.13E-01			
TC2O7							3.48E+01			
TIO2							1.10E-04			
UE3							8.30E+01			
UO3							9.01E-02			
ZNO							2.69E-02			
ZRC2							9.49E-04			

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Table B-9 Phase 1 LAW Mass Balance for Batch PCL/9 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.15E+06				1.61E+06	2.54E+06	2.58E+03	2.58E+03	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	4.15E+06				1.61E+06	2.54E+06	8.62E+03	8.62E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TfU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AP+3									
AS+5									
B+3									
BE+2									
BL+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	7.17E+03				7.17E+03				
CO2	2.81E+05				2.81E+05				
CO3-2									
CR(OH)4-									
CS+									
ClH2									
EU-154									
F-									
F2	3.64E+03				3.64E+03				
FE+3									
H2O	2.54E+06					2.54E+06			
HG+2									
K+									
LA+3									
MD+2									
MN+4									
MO+6									
NA+							4.95E+03	4.95E+03	
NI+3									
NO2	4.60E+05				4.60E+05				
NO2-									
NO3-									
NE+4									
O2	8.55E+05				8.55E+05				1.00E+06
OH-									
PH4							3.66E+03	3.66E+03	
PO4-3									
PU+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TIO4-									
TI+4									
TCC									
UD2+2									
WH+6									
ZN+2									
ZR+4									

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Table B-9 Phase 1 IAW Mass Balance for Batch PCL/9 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		7.54E+05	3.18E+06	3.93E+06					
RADIONUCLIDES (CL)									
Cesium		3.78E+03		3.78E+03					
Strontium		2.52E+04		2.52E+04					
Technetium		3.78E+02		3.78E+02					
TRU		3.20E+02		3.20E+02					
CHEMICALS (kg)									
AGG0		1.33E-09		1.33E-09					
AL2O3		4.89E+04		4.89E+04					
AM2O5		6.09E-02		6.09E-02					
AS2O5		1.10E-09		1.10E-09					
B2O3		1.13E-07		1.13E-07					
BAO		4.25E-04		4.25E-04					
BAO		4.39E-10		4.39E-10					
Bi2O3		6.53E-13		6.53E-13					
CaO		1.17E+03		1.17E+03					
CaO		6.28E-03		6.28E-03					
CaSO3		7.68E+02		7.68E+02					
CaSO		4.62E-02		4.62E-02					
ClO		5.16E-03		5.16E-03					
Bi2O3		6.15E-03		6.15E-03					
Fe2O3		2.82E+02		2.82E+02					
FORMER			3.18E+06	3.18E+06					
HCl		5.93E-03		5.93E-03					
DMAT									
K2O		8.54E+03		8.54E+03					
La2O3		4.76E-03		4.76E-03					
MgO		1.91E-02		1.91E-02					
MnO2		1.04E+02		1.04E+02					
MCO3		4.66E-02		4.66E-02					
Na2O		6.64E+05		6.64E+05					
Ni2O3		9.44E+02		9.44E+02					
NiO2		9.64E-04		9.64E-04					
CH-									
P2O5		6.43E+03		6.43E+03					
PbO2		5.01E+01		5.01E+01					
Flu2		2.06E+00		2.06E+00					
Sb2O3		7.41E-07		7.41E-07					
SiO2		5.52E+00		5.52E+00					
SnO2		1.25E-12		1.25E-12					
SO3		2.24E+04		2.24E+04					
SOLIDS		3.92E+00		3.92E+00					
SR+2									
SrO		2.13E-01		2.13E-01					
TiO2/		3.48E+01		3.48E+01					
TiO2		1.10E-04		1.10E-04					
UO3		8.30E+01		8.30E+01					
UO3		9.01E-02		9.01E-02					
ZnO		2.69E-02		2.69E-02					
ZrO2		9.49E-04		9.49E-04					

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Table B-10 Phase 1 IAW Mass Balance for Batch PCL/10 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.67E+06	3.65E+06	1.72E+04	3.91E+05	4.08E+05		3.65E+06	3.65E+06		
Density (g/L)	1.26E+03	1.26E+03	1.26E+03	1.00E+03	1.01E+03		1.26E+03	1.26E+03		
Total Mass Flow (kg)	4.63E+06	4.61E+06	2.17E+04	3.91E+05	4.13E+05		4.61E+06	4.61E+06		
RADIONUCLIDES (Ci)										
Cesium	3.12E+04	3.11E+04	1.46E+02		1.46E+02		3.11E+04	3.11E+04		
Strontium	9.32E+03	9.28E+03	4.37E+01		4.37E+01		9.28E+03	9.28E+03		
Technetium	3.66E+01	3.64E+01	1.72E-01		1.72E-01		3.64E+01	3.64E+01		
TMI	1.92E+01	1.91E+01	8.98E-02		8.98E-02		1.91E+01	1.91E+01		
CHEMICALS (kg)										
AG+	1.78E-01	1.77E-01	8.35E-04		8.35E-04		1.77E-01	1.77E-01		
AL(OH)4-	1.12E+05	1.11E+05	5.23E+02		5.23E+02		1.11E+05	1.11E+05		
AM+3	3.15E-03	3.13E-03	1.48E-05		1.48E-05		3.13E-03	3.13E-03		
AS+5	9.33E-02	9.27E-02	4.38E-04		4.38E-04		9.27E-02	9.27E-02		
BH3	1.51E-09	1.51E-09	7.09E-12		7.09E-12		1.51E-09	1.51E-09		
BA+2	8.39E-02	8.35E-02	3.93E-04		3.93E-04		8.35E-02	8.35E-02		
BE+2	6.82E-12	6.79E-12	3.20E-14		3.20E-14		6.79E-12	6.79E-12		
BI+3	2.96E-01	2.94E-01	1.39E-03		1.39E-03		2.94E-01	2.94E-01		
C-14	4.55E-04	4.53E-04	2.14E-06		2.14E-06		4.53E-04	4.53E-04		
CA+2	5.24E+01	5.22E+01	2.46E-01		2.46E-01		5.22E+01	5.22E+01		
CD+2	2.07E-01	2.06E-01	9.68E-04		9.68E-04		2.06E-01	2.06E-01		
CL-	4.75E+02	4.73E+02	2.23E+00		2.23E+00		4.73E+02	4.73E+02		
CL2										
CO3-2	9.59E+04	9.53E+04	4.50E+02		4.50E+02		9.53E+04	9.53E+04		
CR(OH)4-	8.10E+01	8.06E+01	3.80E-01		3.80E-01		8.06E+01	8.06E+01		
CS+	3.60E-01	3.59E-01	1.69E-03		1.69E-03		3.59E-01	3.59E-01		
CU+2	7.82E-03	7.78E-03	3.67E-05		3.67E-05		7.78E-03	7.78E-03		
EU-154	3.38E-04	3.36E-04	1.58E-06		1.58E-06		3.36E-04	3.36E-04		
F-	4.66E+03	4.64E+03	2.18E+01		2.18E+01		4.64E+03	4.64E+03		
F2										
FE+3	1.21E+01	1.20E+01	5.67E-02	3.91E+05	5.67E-02		1.20E+01	1.20E+01		
H2O	3.07E+06	3.05E+06	1.44E+04		1.44E+04		3.05E+06	3.05E+06		
HO+2	7.21E-04	7.18E-04	3.38E-06		3.38E-06		7.18E-04	7.18E-04		
IS+	4.49E+02	4.47E+02	2.11E+00		2.11E+00		4.47E+02	4.47E+02		
LA+3	1.89E-04	1.88E-04	8.97E-07		8.97E-07		1.88E-04	1.88E-04		
MD+2	3.81E-01	3.79E-01	1.79E-03		1.79E-03		3.79E-01	3.79E-01		
MN+4	3.48E+00	3.47E+00	1.63E-02		1.63E-02		3.47E+00	3.47E+00		
ND+6	1.37E-01	1.37E-01	6.44E-04		6.44E-04		1.37E-01	1.37E-01		
NA+	5.87E+05	5.84E+05	2.75E+03		2.75E+03		5.84E+05	5.84E+05		
NI+3	4.18E+01	4.16E+01	1.96E-01		1.96E-01		4.16E+01	4.16E+01		
NO2										
NO2-	1.86E+05	1.85E+05	8.71E+02		8.71E+02		1.85E+05	1.85E+05		
NO3-	4.51E+05	4.49E+05	2.12E+03		2.12E+03		4.49E+05	4.49E+05		
NH+4	3.95E-05	3.93E-05	1.83E-07		1.83E-07		3.93E-05	3.93E-05		
O2										
OH-	1.63E+04	1.63E+04	7.66E+01		7.66E+01		1.63E+04	1.63E+04		
PH+4	3.01E+00	2.99E+00	1.41E-02		1.41E-02		2.99E+00	2.99E+00		
PO4-3	1.17E+04	1.16E+04	5.47E+01		5.47E+01		1.16E+04	1.16E+04		
PU+4	1.16E-01	1.15E-01	5.41E-04		5.41E-04		1.15E-01	1.15E-01		
SE+6	5.64E-04	5.62E-04	2.65E-06		2.65E-06		5.62E-04	5.62E-04		
SI+4	1.20E-01	1.20E-01	5.63E-04		5.63E-04		1.20E-01	1.20E-01		
SO4-2	1.88E+04	1.88E+04	8.83E+01		8.83E+01		1.88E+04	1.88E+04		
SR+2	6.71E-02	6.67E-02	3.14E-04		3.14E-04		6.67E-02	6.67E-02		
TDO+	3.54E+00	3.53E+00	1.66E-02		1.66E-02		3.53E+00	3.53E+00		
TI+4	7.15E-03	7.11E-03	3.33E-05		3.33E-05		7.11E-03	7.11E-03		
TCC	8.36E+04	8.32E+04	3.92E+02		3.92E+02		8.32E+04	8.32E+04		
UO2+2	4.05E+00	4.03E+00	1.90E-02		1.90E-02		4.03E+00	4.03E+00		
WH6	3.25E-03	3.23E-03	1.52E-05		1.52E-05		3.23E-03	3.23E-03		
ZM+2	3.70E+00	3.68E+00	1.73E-02		1.73E-02		3.68E+00	3.68E+00		
ZR+4	5.67E-02	5.64E-02	2.66E-04		2.66E-04		5.64E-02	5.64E-02		

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Table B-10 Phase 1 LAW Mass Balance for Batch PCL/10 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.63E+04	4.63E+02	4.59E+04		4.59E+04		4.63E+02	4.63E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
BAO3										
BAC										
BBO										
BL2O3										
CAO										
ClO										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
H2O										
IMHAT										
FeO										
LA2O3										
MO										
MNO2										
MCO3										
NA2O										
NIL2O3										
NEO2										
EO25										
FRG2										
HU2										
SEO3										
SiO2										
SO3										
SOLIDS	4.63E+04	4.63E+02	4.59E+04		4.59E+04		4.63E+02	4.63E+02		
SRO										
TC2O7										
TiO2										
UO3										
W3										
ZNO										
ZK2										

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Table B-10 Phase 1 LAW Mass Balance for Batch PCL/10 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.62E+06	3.06E+03		3.06E+03	3.62E+06	4.74E+06		1.00E-09	1.00E-09
Density (g/L)		1.26E+03	3.34E+03		3.34E+03	1.26E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.61E+06	1.02E+04		1.02E+04	4.61E+06	4.74E+06		1.00E-09	1.00E-09
RADIONUCLIDES (Ci)										
Cesium		4.48E+03	2.66E+04		2.66E+04	4.48E+03				
Strontium		9.28E+03				9.28E+03				
Technetium		3.60E+01	3.66E-01		3.66E-01	3.60E+01				
TU		1.91E+01				1.91E+01				
CHEMICALS (kg)										
AG+		1.77E-01				1.77E-01				
AL(OH)4-		1.11E+05				1.11E+05				
AM+3		3.13E-03				3.13E-03				
AM+5		9.29E-02				9.29E-02				
AP+3		1.51E-09				1.51E-09				
BA+2		8.35E-02				8.35E-02				
BE+2		6.79E-12				6.79E-12				
BI+3		2.94E-01				2.94E-01				
C-14		4.53E-04				4.53E-04				
CA+2		5.22E+01				5.22E+01				
CD+2		2.06E-01				2.06E-01				
CL-		4.73E+02				4.73E+02				
CL2							4.73E+02			
CO2							3.75E+05			
CO3-2		9.55E+04				9.55E+04				
CR(OH)4-		8.06E+01				8.06E+01				
CS+		5.17E-02	3.07E-01		3.07E-01	5.17E-02				
CH2		7.78E-03				7.78E-03				
EJ-154		3.36E-04				3.36E-04				
F-		4.64E+03				4.64E+03				
F2							4.64E+03			
FE+3		1.20E+01				1.20E+01				
H2O		3.05E+06				3.05E+06	3.10E+06		1.00E-09	1.00E-09
HO+2		7.18E-04				7.18E-04				
K+		4.47E+02				4.47E+02				
LA+3		1.88E-04				1.88E-04				
MG+2		3.79E-01				3.79E-01				
MH+4		3.47E+00				3.47E+00				
MO+6		1.37E-01				1.37E-01				
NA+		5.84E+05	5.87E+03		5.87E+03	5.84E+05				
NI+3		4.16E+01				4.16E+01				
NO2							5.18E+05			
NO2-		1.85E+05				1.85E+05				
NO3-		4.49E+05				4.49E+05				
NE+4		3.93E-05				3.93E-05				
O2							7.40E+05			
OH-		1.63E+04	4.34E+03		4.34E+03	1.63E+04				
FB+4		2.99E+00				2.99E+00				
FOA-3		1.16E+04				1.16E+04				
FU+4		1.15E-01				1.15E-01				
SE+6		5.62E-04				5.62E-04				
SI+4		1.20E-01				1.20E-01				
SO4-2		1.88E+04				1.88E+04				
SR+2		6.67E-02				6.67E-02				
TIO4-		3.49E+00	3.54E-02		3.54E-02	3.49E+00				
TI+4		7.11E-03				7.11E-03				
TIC		8.32E+04				8.32E+04				
UO2+2		4.03E+00				4.03E+00				
W+6		3.23E-03				3.23E-03				
ZN+2		3.68E+00				3.68E+00				
ZR+4		5.64E-02				5.64E-02				

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Table B-10 Phase 1 LAW Mass Balance for Batch PCL/10 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.63E+02		5.87E+03	5.87E+03	4.63E+02	8.72E+05			
RADIONUCLIDES (Ci)										
Cesium							4.48E+03			
Strontium							9.28E+03			
Technetium							3.60E+01			
TRU							1.90E+01			
CHEMICALS (kg)										
AC2O							1.90E-01			
AL2O3							5.95E+04			
AM2O3							3.44E-03			
AS2O5							1.43E-01			
B2O3							4.85E-09			
B4O							9.32E-02			
B4O							1.88E-11			
BL2O3							3.28E-01			
CaO							7.30E+01			
ClO							2.35E-01			
CR2O3							5.10E+01			
CS2O							5.47E-02			
CU							9.74E-03			
EU2O3							3.89E-04			
FE2O3							1.72E+01			
FORMER										
H2O							7.75E-04			
IMMAT										
K2O				5.87E+03	5.87E+03					
LA2O3							5.39E+02			
MG							2.21E-04			
MG							6.29E-01			
MNC2							5.48E+00			
MCO3							2.05E-01			
NA2O							7.87E+05			
NIL2O3							5.86E+01			
NEO2							4.46E-05			
PC25							8.68E+03			
PER2							3.46E+00			
PLD2							1.30E-01			
SEB							9.03E-04			
STC2							2.56E-01			
SD3							1.56E+04			
SOLIDS		4.63E+02				4.63E+02				
SFO							7.86E-02			
TC2O7							3.32E+00			
TIC2							1.19E-02			
UD3							4.26E+00			
WD3							4.08E-03			
ZNO							4.58E+00			
ZNC2							7.62E-02			

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Table B-10 Phase 1 LAW Mass Balance for Batch PCL/10 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.74E+06				1.64E+06	3.10E+06	3.06E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	4.74E+06				1.64E+06	3.10E+06	1.02E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
IU									
CHEMICALS (kg)									
AGP									
AL(OH)4-									
AM+3									
AS+5									
BP+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	4.73E+02				4.73E+02				
CO2	3.75E+05				3.75E+05				
CO3-2									
CR(OH)4-									
CS+									
CU+2									
EU-154									
F-									
F2	4.64E+03				4.64E+03				
FE+3									
H2O	3.10E+06					3.10E+06			
HE+2									
K+									
LA+3									
MD+2									
MN+4									
MO+6									
NA+							5.87E+03	5.75E-10	
NI+3									
NO2	5.18E+05				5.18E+05				
NO2-									
NO3-									
NE+4									
O2	7.40E+05				7.40E+05				1.00E+06
OH-									
PH+4							4.34E+03	4.25E-10	
PO4-3									
PU+4									
SE+6									
SI+4									
SO4-2									
SR+2									
TDO+4									
TI+4									
TCC									
UC2+2									
WH6									
ZN+2									
ZR+4									

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Table B-10 Phase 1 LAW Mass Balance for Batch PCL/10 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		8.72E+05	3.79E+06	4.66E+06					
RADIONUCLIDES (Cl)									
Cesium		4.48E+03		4.48E+03					
Strontium		9.28E+03		9.28E+03					
Technetium		3.60E+01		3.60E+01					
TU1		1.90E+01		1.90E+01					
CHEMICALS (kg)									
AC2O		1.90E-01		1.90E-01					
AL2O3		5.95E+04		5.95E+04					
AM2O3		3.44E-03		3.44E-03					
AS2O5		1.43E-01		1.43E-01					
B2O3		4.85E-09		4.85E-09					
B4O		9.32E-02		9.32E-02					
B4O		1.86E-11		1.86E-11					
BIL2O3		3.28E-01		3.28E-01					
CaO		7.30E+01		7.30E+01					
ClO		2.35E-01		2.35E-01					
CR2O3		5.10E+01		5.10E+01					
CS2O		5.47E-02		5.47E-02					
CUO		9.74E-03		9.74E-03					
EU2O3		3.89E-04		3.89E-04					
FE2O3		1.72E+01		1.72E+01					
FORMER			3.79E+06	3.79E+06					
H2O		7.75E-04		7.75E-04					
IMMAT									
K2O		5.39E+02		5.39E+02					
LA2O3		2.21E-04		2.21E-04					
MO		6.29E-01		6.29E-01					
MND2		5.48E+00		5.48E+00					
MCO3		2.05E-01		2.05E-01					
NA2O		7.87E+05		7.87E+05					
NI2O3		5.86E+01		5.86E+01					
NEO2		4.46E-05		4.46E-05					
PE2O5		8.68E+03		8.68E+03					
PEO2		3.46E+00		3.46E+00					
PIO2		1.30E-01		1.30E-01					
SEO3		9.03E-04		9.03E-04					
STO2		2.56E-01		2.56E-01					
SO3		1.56E+04		1.56E+04					
SOLIDS		4.63E+02		4.63E+02					
SFO		7.86E-02		7.86E-02					
TCCO7		3.32E+00		3.32E+00					
TIO2		1.19E-02		1.19E-02					
UC3		4.26E+00		4.26E+00					
UC3		4.08E-03		4.08E-03					
ZNO		4.58E+00		4.58E+00					
ZRO2		7.62E-02		7.62E-02					

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Table B-11 Phase 1 LAW Mass Balance for Batch PCL/11 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.65E+06	3.64E+06	1.71E+04	3.89E+05	4.06E+05		3.64E+06	3.63E+06	1.71E+02	3.89E+03
Density (g/L)	1.26E+03	1.26E+03	1.26E+03	1.00E+03	1.01E+03		1.26E+03	1.26E+03	1.26E+03	1.00E+03
Total Mass Flow (kg)	4.61E+06	4.59E+06	2.16E+04	3.89E+05	4.10E+05		4.59E+06	4.59E+06	2.16E+02	3.89E+03
RADIONUCLIDES (Ci)										
Cesium	4.10E+04	4.08E+04	1.92E+02		1.92E+02		4.08E+04	4.08E+04	1.92E+00	
Strontium	4.40E+04	4.38E+04	2.05E+02		2.05E+02		4.38E+04	4.38E+04	1.99E+00	
Technetium	7.22E+01	7.19E+01	3.38E-01		3.38E-01		7.19E+01	7.19E+01	3.38E-03	
IU1	1.00E+01	9.96E+00	4.68E-02		4.68E-02		9.96E+00	9.95E+00	4.68E-04	
CHEMICALS (kg)										
AGH	1.05E-01	1.05E-01	4.94E-04		4.94E-04		1.05E-01	1.05E-01	4.94E-06	
AL(OH)4-	1.10E+05	1.09E+05	5.14E+02		5.14E+02		1.09E+05	1.09E+05	5.14E+00	
AMH3	2.00E-03	2.04E-03	9.59E-06		9.59E-06		2.04E-03	2.04E-03	9.59E-08	
ASH5	9.33E-02	9.29E-02	4.37E-04		4.37E-04		9.29E-02	9.29E-02	4.37E-06	
BH3	9.83E-01	9.82E-01	4.63E-02		4.63E-02		9.80E-01	9.80E-01	4.63E-05	
BH2	1.39E+00	1.39E+00	6.52E-03		6.52E-03		1.39E+00	1.38E+00	6.52E-05	
BEH2	2.29E-13	2.28E-13	1.07E-15		1.07E-15		2.28E-13	2.28E-13	1.07E-17	
BIH3	1.64E-01	1.63E-01	7.69E-04		7.69E-04		1.63E-01	1.63E-01	7.69E-06	
C-14	2.06E-05	2.05E-05	9.63E-08		9.63E-08		2.05E-05	2.05E-05	9.63E-10	
CAH2	5.29E+01	5.26E+01	2.48E-01		2.48E-01		5.26E+01	5.26E+01	2.48E-03	
CDH2	1.96E-01	1.95E-01	9.19E-04		9.19E-04		1.95E-01	1.95E-01	9.19E-06	
CL-	2.43E+02	2.42E+02	1.14E+00		1.14E+00		2.42E+02	2.42E+02	1.14E-02	
CL2										
CO3-2										
CO3(OH)4-	9.42E+04	9.37E+04	4.41E+02		4.41E+02		9.37E+04	9.37E+04	4.41E+00	
CS-	4.23E+01	4.21E+01	1.98E-01		1.98E-01		4.21E+01	4.21E+01	1.98E-03	
CSH	4.74E-01	4.71E-01	2.22E-03		2.22E-03		4.71E-01	4.71E-01	2.22E-05	
CH2	4.26E-03	4.24E-03	2.00E-05		2.00E-05		4.24E-03	4.24E-03	2.00E-07	
EU-154	1.35E-05	1.34E-05	6.31E-08		6.31E-08		1.34E-05	1.34E-05	6.31E-10	
F-	4.63E+03	4.61E+03	2.17E+01		2.17E+01		4.61E+03	4.61E+03	2.17E-01	
F2										
FEH3	4.40E+00	4.38E+00	2.06E-02		2.06E-02		4.38E+00	4.38E+00	2.06E-04	
H2O	3.05E+06	3.04E+06	1.43E+04	3.89E+05	4.03E+05		3.04E+06	3.04E+06	1.43E+02	3.89E+03
H3H2	2.71E-04	2.70E-04	1.27E-06		1.27E-06		2.70E-04	2.70E-04	1.27E-08	
HS-	1.58E+03	1.57E+03	7.41E+00		7.41E+00		1.57E+03	1.57E+03	7.41E-02	
IAlH3	1.39E+01	1.39E+01	6.52E-02		6.52E-02		1.39E+01	1.38E+01	6.52E-04	
MDH2	3.67E+00	3.66E+00	1.72E-02		1.72E-02		3.66E+00	3.66E+00	1.72E-04	
MH4	3.07E-01	3.05E-01	1.44E-03		1.44E-03		3.05E-01	3.05E-01	1.44E-05	
MDH6	8.31E-02	8.27E-02	3.89E-04		3.89E-04		8.27E-02	8.27E-02	3.89E-06	
NA+	5.84E+05	5.81E+05	2.74E+03		2.74E+03		5.81E+05	5.81E+05	2.74E+01	
NIH3	1.63E+01	1.63E+01	7.65E-02		7.65E-02		1.63E+01	1.63E+01	7.65E-04	
NO2										
NO2-	1.83E+05	1.82E+05	8.58E+02		8.58E+02		1.82E+05	1.82E+05	8.58E+00	
NO3-	4.49E+05	4.47E+05	2.10E+03		2.10E+03		4.47E+05	4.47E+05	2.10E+01	
NIH4	1.38E-06	1.38E-06	6.47E-09		6.47E-09		1.38E-06	1.38E-06	6.47E-11	
O2										
OH-	1.94E+04	1.93E+04	9.06E+01		9.06E+01		1.93E+04	1.93E+04	9.06E-01	
FBH4	8.52E-01	8.48E-01	3.99E-03		3.99E-03		8.48E-01	8.48E-01	3.99E-05	
FOH-3	1.15E+04	1.14E+04	5.38E+01		5.38E+01		1.14E+04	1.14E+04	5.38E-01	
FUH4	4.11E-02	4.09E-02	1.93E-04		1.93E-04		4.09E-02	4.09E-02	1.93E-06	
SEH6	6.82E-03	6.79E-03	3.19E-05		3.19E-05		6.79E-03	6.79E-03	3.19E-07	
SIH4	7.40E+00	7.37E+00	3.47E-02		3.47E-02		7.37E+00	7.37E+00	3.47E-04	
SOH-2	1.88E+04	1.88E+04	8.82E+01		8.82E+01		1.88E+04	1.88E+04	8.82E-01	
SRH2	3.16E-01	3.15E-01	1.48E-03		1.48E-03		3.15E-01	3.15E-01	1.48E-05	
TDOH4	7.00E+00	6.97E+00	3.28E-02		3.28E-02		6.97E+00	6.97E+00	3.28E-04	
TIH4	3.98E-03	3.96E-03	1.87E-05		1.87E-05		3.96E-03	3.96E-03	1.87E-07	
TCU	8.29E+04	8.26E+04	3.89E+02		3.89E+02		8.26E+04	8.26E+04	3.89E+00	
UDH2	1.16E+01	1.16E+01	5.44E-02		5.44E-02		1.16E+01	1.16E+01	5.44E-04	
WH6	1.12E-04	1.12E-04	5.26E-07		5.26E-07		1.12E-04	1.12E-04	5.26E-09	
ZNH2	7.26E+00	7.22E+00	3.40E-02		3.40E-02		7.22E+00	7.22E+00	3.40E-04	
ZRH4	3.15E-02	3.14E-02	1.48E-04		1.48E-04		3.14E-02	3.14E-02	1.48E-06	

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Table B-11 Phase 1 LAW Mass Balance for Batch PCL/11 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.61E+04	4.61E+02	4.56E+04		4.56E+04		4.61E+02	4.61E+00	4.56E+02	
RADIONUCLIDES (Cl)										
Cesium							1.42E+04	1.42E+02	1.41E+04	
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
BC2B										
BAO										
BD										
BL2O3										
CAO										
CO										
CR2O3										
CS2O										
CU										
EU2O3										
FE2O3										
FORMER										
H2O										
IMPAT										
K2O										
LA2O3										
MO										
MO2										
MCO3										
NA2O										
NL2O3										
NEO2										
OH-							3.86E-02	3.86E-04	3.82E-02	
P2O5										
PBO2										
PUC2										
SBO3										
SI02										
SO3										
SOLIDS	4.61E+04	4.61E+02	4.56E+04		4.56E+04		4.61E+02	4.61E+00	4.56E+02	
SR+2							1.02E-01	1.02E-03	1.01E-01	
SRO										
TC2O7										
TIO2										
U3										
UC3										
ZNO										
ZRO2										

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Table B-11 Phase 1 LAW Mass Balance for Batch PCL/11 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	4.06E+03	3.63E+06	3.05E+03		3.05E+03	3.63E+06	4.72E+06		1.00E-09	1.00E-09
Density (g/L)	1.01E+03	1.26E+03	3.34E+03		3.34E+03	1.26E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)										
	4.10E+03	4.59E+06	1.02E+04		1.02E+04	4.59E+06	4.72E+06		1.00E-09	1.00E-09
RADIOISOTOPES (Ci)										
Cesium	1.92E+00	4.46E+03	3.64E+04		3.64E+04	4.46E+03				
Strontium	1.39E+00	2.96E+04				2.96E+04				
Technetium	3.38E-03	7.12E+01	7.23E-01		7.23E-01	7.12E+01				
IU1	4.68E-04	9.95E+00				9.95E+00				
CHEMICALS (kg)										
ACF	4.94E-06	1.03E-01				1.05E-01				
AL(CH ₃) ₄	5.14E+00	1.09E+05				1.09E+05				
AM#3	9.59E-08	2.04E-03				2.04E-03				
ASH#5	4.37E-06	9.29E-02				9.29E-02				
BP#3	4.61E-05	9.80E-01				9.80E-01				
BE#2	6.52E-05	1.38E+00				1.38E+00				
BE#2	1.07E-17	2.28E-13				2.28E-13				
BI#3	7.69E-06	1.63E-01				1.63E-01				
C-14	9.63E-10	2.05E-05				2.05E-05				
CA#2	2.48E-03	5.26E+01				5.26E+01				
CD#2	9.19E-06	1.95E-01				1.95E-01				
CL-	1.14E-02	2.42E+02				2.42E+02				
CL2							2.42E+02			
CO2							3.71E+05			
CO3-2	4.41E+00	9.37E+04				9.37E+04				
CR(CH ₃) ₄	1.98E-03	4.21E+01				4.21E+01				
CSH	2.22E-05	5.14E-02	4.20E-01		4.20E-01	5.14E-02				
CI#2	2.00E-07	4.24E-03				4.24E-03				
EJ-154	6.31E-10	1.34E-05				1.34E-05				
F-	2.17E-01	4.61E+03				4.61E+03				
F2							4.61E+03			
FE#3	2.06E-04	4.38E+00				4.38E+00				
H2O	4.03E+03	3.04E+06				3.04E+06		3.09E+06		
HG#2	1.27E-08	2.70E-04				2.70E-04				
NI	7.41E-02	1.57E+03				1.57E+03				
LA#3	6.52E-04	1.38E+01				1.38E+01				
NE#2	1.72E-04	3.66E+00				3.66E+00				
NH#4	1.44E-05	3.05E-01				3.05E-01				
ND#6	3.89E-06	8.27E-02				8.27E-02				
NA#	2.74E+01	5.81E+05	5.84E+03		5.84E+03	5.81E+05				
NI#3	7.65E-04	1.63E+01				1.63E+01				
NO2							5.14E+05			
NO2-	8.58E+00	1.82E+05				1.82E+05				
NO3-	2.10E+01	4.47E+05				4.47E+05				
NO#4	6.47E-11	1.38E-06				1.38E-06				
O2							7.42E+05			
OH-	9.06E-01	1.93E+04	4.32E+03		4.32E+03	1.93E+04				
CH ₃	3.99E-05	8.48E-01				8.48E-01				
EB#4	5.38E-01	1.14E+04				1.14E+04				
FO#-3	1.93E-06	4.09E-02				4.09E-02				
FI#4	3.19E-07	6.79E-03				6.79E-03				
SE#6	3.47E-04	7.37E+00				7.37E+00				
SI#4	8.82E-01	1.88E+04				1.88E+04				
SO#-2	1.00E-05	2.13E-01				2.13E-01				
SR#2	3.28E-04	6.90E+00	7.00E-02		7.00E-02	6.90E+00				
TIC#4	1.87E-07	3.96E-03				3.96E-03				
TIC2	3.89E+00	8.26E+04				8.26E+04				
UD#2	5.44E-04	1.16E+01				1.16E+01				
W#6	5.26E-09	1.12E-04				1.12E-04				
ZN#2	3.40E-04	7.22E+00				7.22E+00				
ZR#4	1.48E-06	3.14E-02				3.14E-02				

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Table B-11 Phase 1 LAW Mass Balance for Batch PCL/11 (6 sheets)

STREAM NAME SOLID COMPONENTS	11	12	13	14	15	16	16A	17	18	19
Total Mass Flow (kg)	4.56E+02	4.61E+00		5.84E+03	5.84E+03	4.61E+00	8.68E+05			
RADIONUCLIDES (Ci)										
Cesium										
Strontium	1.41E+04	1.42E+02								
Technetium						1.42E+02	4.46E+03			
TRU							2.97E+04			
							7.12E+01			
							9.92E+00			
CHEMICALS (kg)										
AG2O							1.13E-01			
AL2O3							5.86E+04			
AM2O3							2.24E-03			
AS2O5							1.43E-01			
BAO3							3.16E+00			
BAO							1.53E+00			
BBO							6.32E-13			
BI2O3							1.82E-01			
CaO							7.35E+01			
CaO							2.23E-01			
CR2O3							2.66E+01			
CS2O							5.45E-02			
CUO							5.31E-03			
EU2O3							1.55E-05			
FE2O3							6.26E+00			
FORMER										
H2O							2.92E-04			
DMFAT				5.84E+03	5.84E+03					
K2O							1.90E+03			
LA2O3							1.62E+01			
MgO							6.06E+00			
MNO2							4.83E-01			
MCO3							1.24E-01			
NA2O							7.84E+05			
NIL2O3							2.29E+01			
NEO2							1.56E-06			
OH-	3.82E-02	3.86E-04								
PO5							3.86E-04			
PBO2							8.55E+03			
HUC2							9.79E-01			
SBO3							4.64E-02			
SBO3							1.09E-02			
SiO2							1.58E+01			
SO3							1.56E+04			
SOLIDS							4.61E+00			
SR+2	4.56E+02	4.61E+00					4.61E+00			
SRO	1.01E-01	1.02E-03					1.02E-03			
TC2O7							2.52E-01			
TiO2							6.56E+00			
UO3							6.61E-03			
UO3							1.23E+01			
VO3							1.41E-04			
ZNO							8.99E+00			
ZRC2							4.24E-02			

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Table B-11 Phase 1 LAW Mass Balance for Batch PCL/11 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.72E+06				1.63E+06	3.09E+06	3.05E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	4.72E+06				1.63E+06	3.09E+06	1.02E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
IU1									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
BA+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	2.42E+02				2.42E+02				
CO2	3.71E+05				3.71E+05				
CO3-2									
CR(OH)4-									
CS+									
CI+2									
EJ-154									
F-									
F2	4.61E+03				4.61E+03				
FE+3						3.09E+06			
H2O	3.09E+06								
HO+2									
K+									
LA+3									
ME+2									
MN+4									
MO+6									
NA+							5.84E+03	5.75E-10	
NI+3									
NO2	5.14E+05				5.14E+05				
NO2-									
NO3-									
NO+4									
O2	7.42E+05				7.42E+05				1.00E+06
OH-									
OH+4							4.32E+03	4.25E-10	
PO4-3									
PU+4									
SE+6									
SI+4									
SO4-2									
SR+2									
TIO4-									
TI+4									
TIC									
UO2+2									
WH6									
ZN+2									
ZR+4									

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Table B-11 Phase 1 LAW Mass Balance for Batch PCL/11 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		8.68E+05	3.77E+06	4.64E+06					
RADIONUCLIDES (Cl.)									
Cesium		4.46E+03		4.46E+03					
Strontium		2.97E+04		2.97E+04					
Technetium		7.12E+01		7.12E+01					
TU		9.92E+00		9.92E+00					
CHEMICALS (kg)									
AG2O		1.13E-01		1.13E-01					
AL2O3		5.86E+04		5.86E+04					
AM2O3		2.24E-03		2.24E-03					
AS2O3		1.43E-01		1.43E-01					
B2O3		3.16E+00		3.16E+00					
B4O7		1.53E+00		1.53E+00					
B2O		6.32E-13		6.32E-13					
Bi2O3		1.82E-01		1.82E-01					
CaO		7.36E+01		7.36E+01					
ClO		2.23E-01		2.23E-01					
CR2O3		2.66E+01		2.66E+01					
CS2O		5.45E-02		5.45E-02					
CUO		5.31E-03		5.31E-03					
EU2O3		1.53E-05		1.53E-05					
FE2O3		6.26E+00		6.26E+00					
FURMER			3.77E+06	3.77E+06					
H2O		2.92E-04		2.92E-04					
HMPT									
K2O		1.90E+03		1.90E+03					
LA2O3		1.62E+01		1.62E+01					
M2O		6.06E+00		6.06E+00					
MnO2		4.83E-01		4.83E-01					
MO3		1.24E-01		1.24E-01					
Na2O		7.84E+05		7.84E+05					
NI2O3		2.29E+01		2.29E+01					
NiO2		1.56E-06		1.56E-06					
OH-									
PO5		8.53E+03		8.53E+03					
PO2		9.79E-01		9.79E-01					
RU2		4.64E-02		4.64E-02					
SEO3		1.09E-02		1.09E-02					
SiO2		1.58E+01		1.58E+01					
SO3		1.56E+04		1.56E+04					
SOLIDS		4.61E+00		4.61E+00					
SR+2									
SrO		2.52E-01		2.52E-01					
TC2O7		6.56E+00		6.56E+00					
TiO2		6.61E-03		6.61E-03					
U3		1.23E+01		1.23E+01					
UO3		1.41E-04		1.41E-04					
ZNO		8.99E+00		8.99E+00					
ZrO2		4.24E-02		4.24E-02					

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Table B-12 Phase 1 LAW Mass Balance for Batch PCL/12 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	1.79E+06	1.78E+06	1.18E+04	1.87E+05	1.99E+05		1.78E+06	1.78E+06		
Density (g/L)	1.27E+03	1.27E+03	1.27E+03	1.00E+03	1.02E+03		1.27E+03	1.27E+03		
Total Mass Flow (kg)	2.27E+06	2.25E+06	1.50E+04	1.87E+05	2.02E+05		2.25E+06	2.25E+06		
RADIOISOTOPES (Ci)										
Cesium	3.05E+06	3.03E+06	2.01E+04		2.01E+04		3.03E+06	3.03E+06		
Strontium	8.37E+03	8.32E+03	5.32E+01		5.32E+01		8.32E+03	8.32E+03		
Technetium	6.15E+02	6.11E+02	4.05E+00		4.05E+00		6.11E+02	6.11E+02		
IU	6.21E+01	6.17E+01	4.10E-01		4.10E-01		6.17E+01	6.17E+01		
CHEMICALS (kg)										
AG+	5.32E-03	5.29E-03	3.51E-05		3.51E-05		5.29E-03	5.29E-03		
AL(OH)4-	4.72E+04	4.69E+04	3.11E+02		3.11E+02		4.69E+04	4.69E+04		
AP+3	9.94E-03	9.87E-03	6.53E-05		6.53E-05		9.87E-03	9.87E-03		
AP+5	4.78E-03	4.73E-03	3.15E-05		3.15E-05		4.73E-03	4.73E-03		
B+3	5.09E-02	5.06E-02	3.36E-04		3.36E-04		5.06E-02	5.06E-02		
BA+2	1.56E-01	1.55E-01	1.03E-03		1.03E-03		1.55E-01	1.55E-01		
BI+3	8.29E-03	8.24E-03	5.47E-05		5.47E-05		8.24E-03	8.24E-03		
C-14	6.96E-04	6.91E-04	4.59E-06		4.59E-06		6.91E-04	6.91E-04		
CA+2	5.73E+00	5.69E+00	3.78E-02		3.78E-02		5.69E+00	5.69E+00		
CD+2	1.00E-02	9.96E-03	6.61E-05		6.61E-05		9.96E-03	9.96E-03		
CL-	2.35E+02	2.34E+02	1.55E+00		1.55E+00		2.34E+02	2.34E+02		
CL2										
CO2										
CO3-2	7.08E+04	7.03E+04	4.67E+02		4.67E+02		7.03E+04	7.03E+04		
CR(OH)4-	4.13E+03	4.10E+03	2.72E+01		2.72E+01		4.10E+03	4.10E+03		
CS+	3.53E+01	3.50E+01	2.33E-01		2.33E-01		3.50E+01	3.50E+01		
CU+2	2.14E-04	2.13E-04	1.41E-06		1.41E-06		2.13E-04	2.13E-04		
EU-154	1.83E-02	1.82E-02	1.21E-04		1.21E-04		1.82E-02	1.82E-02		
F-	3.25E+03	3.23E+03	2.14E+01		2.14E+01		3.23E+03	3.23E+03		
F2										
FE+3	3.65E-01	3.62E-01	2.40E-03	1.87E+05	2.40E-03		3.62E-01	3.62E-01		
H2O	1.62E+06	1.61E+06	1.07E+04		1.98E+05		1.61E+06	1.61E+06		
HP+2	1.36E-05	1.35E-05	8.93E-09		8.93E-09		1.35E-05	1.35E-05		
K+	5.12E+03	5.08E+03	3.37E+01		3.37E+01		5.08E+03	5.08E+03		
LA+3	1.62E+00	1.61E+00	1.07E-02		1.07E-02		1.61E+00	1.61E+00		
MA+2	3.84E-01	3.81E-01	2.53E-03		2.53E-03		3.81E-01	3.81E-01		
MA+4	1.35E-02	1.34E-02	8.89E-05		8.89E-05		1.34E-02	1.34E-02		
MD+6	4.20E-03	4.17E-03	2.77E-05		2.77E-05		4.17E-03	4.17E-03		
Na+	2.04E+05	2.03E+05	1.35E+03		1.35E+03		2.03E+05	2.03E+05		
NI+3	1.73E+00	1.72E+00	1.14E-02		1.14E-02		1.72E+00	1.72E+00		
NO2										
NO2-	1.09E+05	1.08E+05	7.18E+02		7.18E+02		1.08E+05	1.08E+05		
NO3-	1.31E+05	1.30E+05	8.60E+02		8.60E+02		1.30E+05	1.30E+05		
NO4-	1.85E-01	1.84E-01	1.22E-03		1.22E-03		1.84E-01	1.84E-01		
O2										
OH-	1.73E+04	1.72E+04	1.14E+02		1.14E+02		1.72E+04	1.72E+04		
PB+4	4.20E-02	4.17E-02	2.77E-04		2.77E-04		4.17E-02	4.17E-02		
FO4-3	2.24E+03	2.22E+03	1.48E+01		1.48E+01		2.22E+03	2.22E+03		
FU+4	3.85E-01	3.83E-01	2.54E-03		2.54E-03		3.83E-01	3.83E-01		
SE+6	3.52E-04	3.49E-04	2.32E-06		2.32E-06		3.49E-04	3.49E-04		
SI+4	5.49E+02	5.45E+02	3.62E+00		3.62E+00		5.45E+02	5.45E+02		
SO4-2	3.80E+04	3.78E+04	2.51E+02		2.51E+02		3.78E+04	3.78E+04		
SR+2	6.02E-02	5.99E-02	3.97E-04		3.97E-04		5.99E-02	5.99E-02		
TCM+	5.95E+01	5.91E+01	3.93E-01		3.93E-01		5.91E+01	5.91E+01		
TI+4	2.00E-04	1.99E-04	1.32E-06		1.32E-06		1.99E-04	1.99E-04		
TCC	7.20E+03	7.15E+03	4.75E+01		4.75E+01		7.15E+03	7.15E+03		
UD+2	3.39E+03	3.37E+03	2.24E+01		2.24E+01		3.37E+03	3.37E+03		
W+6	3.60E-06	3.58E-06	2.38E-08		2.38E-08		3.58E-06	3.58E-06		
ZM+2	5.31E-01	5.27E-01	3.50E-03		3.50E-03		5.27E-01	5.27E-01		
ZR+4	1.59E-03	1.58E-03	1.05E-05		1.05E-05		1.58E-03	1.58E-03		

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Table B-12 Phase 1 LAW Mass Balance for Batch PCL/L2 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	2.26E+04	2.26E+02	2.24E+04		2.24E+04		2.26E+02	2.26E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
AL2O3										
AL2O3										
AS2O5										
B2O3										
B4O7										
Bi2O3										
CaO										
ClO2										
CR2O3										
CS2O										
ClO										
EU2O3										
FE2O3										
FORMER										
H2O										
DRYHT										
K2O										
LA2O3										
MgO										
MnO2										
MOO3										
Na2O										
Ni2O3										
NEO2										
FeO5										
PEO2										
RUO2										
SEO3										
SiO2										
SiO										
SOLIDS	2.26E+04	2.26E+02	2.24E+04		2.24E+04		2.26E+02	2.26E+02		
SiO										
Ta2O7										
TiO2										
UO3										
W3										
ZnO										
ZrO2										

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Table B-12 Phase 1 LAW Mass Balance for Batch PCL/L2 (6 sheets)

STREAM NAME LIQUID COMPONENTS	11	12	13	14	15	16	16A	17	18	19
Volume (L)		1.78E+06	1.10E+03		1.10E+03	1.78E+06	2.91E+06	1.09E+03	2.04E+03	3.12E+03
Density (g/L)		1.27E+03	3.26E+03		3.26E+03	1.27E+03	1.00E+03	3.29E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)		2.25E+06	3.58E+03		3.58E+03	2.25E+06	2.91E+06	3.57E+03	2.04E+03	5.61E+03

RADIONUCLIDES (Ci)										
Cesium		3.89E+03	3.03E+06		3.03E+06	3.89E+03				
Strontium		8.32E+03				8.32E+03				
Technetium		6.03E+02	6.15E+00		6.15E+00	3.89E+02		2.16E+02		2.16E+02
TU		6.17E+01				6.17E+01				

CHEMICALS (kg)										
AG+		5.29E-03				5.29E-03				
AL(OH)4-		4.69E+04				4.69E+04				
AM#3		9.87E-03				9.87E-03				
AS+5		4.73E-03				4.73E-03				
B#3		5.04E-02				5.04E-02				
B#42		1.53E-01				1.53E-01				
BI+3		8.24E-03				8.24E-03				
C-14		6.91E-04				6.91E-04				
CA+2		5.69E+00				5.69E+00				
CD+2		9.96E-03				9.96E-03				
CL-		2.34E+02				2.34E+02				
CL2							2.34E+02			
CO2							7.78E+04			
CO3-2		7.03E+04				7.03E+04				
CR(OH)4-		4.10E+03				4.10E+03				
CS+		4.49E-02				4.49E-02				
CH2		2.13E-04				2.13E-04				
EU-154		1.82E-02				1.82E-02				
F-		3.23E+03				3.23E+03				
F2							3.23E+03			
FE+3		3.62E-01				3.62E-01				
H2O		1.61E+06				1.61E+06	1.64E+06		2.04E+03	2.04E+03
H3+2		1.35E-05				1.35E-05				
K+		5.08E+03				5.08E+03				
LA+3		1.61E+00				1.61E+00				
MP+2		3.81E-01				3.81E-01				
M#4		1.34E-02				1.34E-02				
MD+6		4.17E-03				4.17E-03				
NA+		2.03E+05	2.04E+03		2.04E+03	2.03E+05		2.04E+03		2.04E+03
NI+3		1.72E+00				1.72E+00				
NO2							2.04E+05			
NO2-		1.08E+05				1.08E+05				
NO3-		1.30E+05				1.30E+05				
NP+4		1.84E-01				1.84E-01				
OE							9.80E+05			
OH-		1.72E+04	1.51E+03		1.51E+03	1.72E+04		1.51E+03		1.51E+03
OH#4		4.17E-02				4.17E-02				
PO4-3		2.22E+03				2.22E+03				
PU+4		3.83E-01				3.83E-01				
SE+6		3.49E-04				3.49E-04				
SI+4		5.45E+02				5.45E+02				
SO4-2		3.78E+04				3.78E+04				
SR+2		5.98E-02				5.98E-02				
TO#4-		5.83E+01	5.95E-01		5.95E-01	3.77E+01		2.09E+01		2.09E+01
TI+4		1.99E-04				1.99E-04				
TIC		7.15E+03				7.15E+03				
UC#2		3.37E+03				3.37E+03				
W#6		3.58E-06				3.58E-06				
ZH#2		5.27E-01				5.27E-01				
ZR+4		1.58E-03				1.58E-03				

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Table B-12 Phase 1 LAW Mass Balance for Batch PCL/12 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		2.26E+02		2.04E+03	2.04E+03	2.26E+02	3.45E+05			
RADIONUCLIDES (Cl)										
Cesium							3.89E+03			
Strontium							8.32E+03			
Technetium							3.89E+02			
TRU							6.14E+01			
CHEMICALS (kg)										
AG2O							5.68E-03			
AL2O3							2.52E+04			
AM2O3							1.09E-02			
AS2O5							7.28E-03			
B2O3							1.63E-01			
B4O							1.73E-01			
BL2O3							9.19E-03			
CaO							7.96E+00			
ClO							1.14E-02			
CR2O3							2.60E+03			
CS2O							4.75E-02			
ClO							2.67E-04			
EU2O3							2.11E-02			
FE2O3							5.18E-01			
FORMER										
H2O							1.46E-05			
DMFAT										
K2O				2.04E+03	2.04E+03		6.12E+03			
LA2O3							1.88E+00			
M2O							6.32E-01			
MN2							2.12E-02			
MO3							6.26E-03			
Na2O							2.73E+05			
NL2O3							2.42E+00			
NF2							2.09E-01			
PCO5							1.66E+03			
PCO2							4.82E-02			
PL2							4.34E-01			
SE3O							5.62E-04			
SiO2							1.17E+03			
SO3							3.15E+04			
SOLIDS		2.26E+02					2.26E+02			
SrO							7.05E-02			
TC2O7							3.58E+01			
TI2							3.32E-04			
UO3							3.57E+03			
W3							4.51E-06			
ZnO							6.56E-01			
ZrO2							2.13E-03			

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Table B-12 Phase 1 LAW Mass Balance for Batch PCL/12 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	2.91E+06				1.27E+06	1.64E+06	1.06E+03	1.06E+03	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	2.91E+06				1.27E+06	1.64E+06	3.55E+03	3.55E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
As+3									
As+5									
BH3									
BH2									
BH3									
C-14									
Ca+2									
CD+2									
CL-									
CL2	2.34E+02				2.34E+02				
CO2	7.78E+04				7.78E+04				
CO3-2									
CR(OH)4-									
CS+									
CU+2									
EU-154									
F-									
F2	3.23E+03				3.23E+03				
FE+3									
H2O	1.64E+06					1.64E+06			
H2O2									
K+									
LA+3									
MH2									
MH4									
MD+6									
NA+							2.04E+03	2.04E+03	
NI+3									
NO2	2.04E+05				2.04E+05				
NO2-									
NO3-									
NO3+									
CO2	9.80E+05				9.80E+05				
OH-									
OH4							1.51E+03	1.51E+03	1.00E+06
FO4-3									
FU+4									
SE+6									
SI+4									
SO4-2									
SR+2									
TIO4-									
TI+4									
TIC									
UO2H2									
W+6									
ZH+2									
ZR+4									

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Table B-12 Phase 1 LAW Mass Balance for Batch PCL/12 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		3.43E+05	3.71E+06	4.05E+06					
RADIONUCLIDES (Cl)									
Cesium		3.89E+03		3.89E+03					
Strontium		8.32E+03		8.32E+03					
Technetium		3.89E+02		3.89E+02					
TRU		6.14E+01		6.14E+01					
CHEMICALS (kg)									
AC2O		5.68E-03		5.68E-03					
AL2O3		2.52E+04		2.52E+04					
AM2O3		1.09E-02		1.09E-02					
AS2O5		7.28E-03		7.28E-03					
B2O3		1.63E-01		1.63E-01					
BAO		1.73E-01		1.73E-01					
BL2O3		9.19E-03		9.19E-03					
CaO		7.96E+00		7.96E+00					
ClO		1.14E-02		1.14E-02					
CR2O3		2.60E+03		2.60E+03					
CS2O		4.75E-02		4.75E-02					
ClO		2.67E-04		2.67E-04					
EU2O3		2.11E-02		2.11E-02					
FE2O3		5.18E-01		5.18E-01					
FORMER			3.71E+06						
H2O		1.46E-05		1.46E-05					
DEWAT									
K2O		6.12E+03		6.12E+03					
LA2O3		1.88E+00		1.88E+00					
M2O		6.32E-01		6.32E-01					
MN2		2.12E-02		2.12E-02					
MO3		6.26E-03		6.26E-03					
NA2O		2.73E+05		2.73E+05					
NL2O3		2.42E+00		2.42E+00					
NF2		2.09E-01		2.09E-01					
PA2O5		1.66E+03		1.66E+03					
PR2		4.82E-02		4.82E-02					
RU2		4.34E-01		4.34E-01					
SE3		5.62E-04		5.62E-04					
SiO2		1.17E+03		1.17E+03					
SO3		3.15E+04		3.15E+04					
SOLIDS		2.26E+02		2.26E+02					
SRO		7.05E-02		7.05E-02					
TC2O7		3.58E+01		3.58E+01					
TI2		3.32E-04		3.32E-04					
U3		3.57E+03		3.57E+03					
VO3		4.51E-06		4.51E-06					
ZNO		6.56E-01		6.56E-01					
ZR2		2.13E-03		2.13E-03					

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Table B-13 Phase 1 LAW Mass Balance for Batch PC2/13 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.36E+06	3.35E+06	1.71E+04	4.02E+05	4.19E+05		3.35E+06	3.35E+06		
Density (g/L)	1.42E+03	1.42E+03	1.42E+03	1.00E+03	1.02E+03		1.42E+03	1.42E+03		
Total Mass Flow (kg)	4.79E+06	4.77E+06	2.44E+04	4.02E+05	4.27E+05		4.77E+06	4.77E+06		
RADIONUCLIDES (Ci)										
Cesium	1.01E+06	1.01E+06	5.14E+03		5.14E+03		1.01E+06	1.01E+06		
Strontium	6.47E+03	6.44E+03	3.23E+01		3.23E+01		6.44E+03	6.44E+03		
Technetium	2.62E+02	2.61E+02	1.33E+00		1.33E+00		2.61E+02	2.61E+02		
TU	2.39E+01	2.37E+01	1.21E-01		1.21E-01		2.37E+01	2.37E+01		
CHEMICALS (kg)										
AG+	2.64E-12	2.63E-12	1.35E-14		1.35E-14		2.63E-12	2.63E-12		
AL(OH)4-	3.34E+05	3.33E+05	1.70E+03		1.70E+03		3.33E+05	3.33E+05		
AM+3	8.81E-04	8.77E-04	4.48E-06		4.48E-06		8.77E-04	8.77E-04		
AS+5	2.64E-13	2.63E-13	1.35E-15		1.35E-15		2.63E-13	2.63E-13		
B+3	8.33E-07	8.27E-07	4.22E-09		4.22E-09		8.27E-07	8.27E-07		
BA+2	1.59E-02	1.57E-02	8.04E-05		8.04E-05		1.57E-02	1.57E-02		
BE+2	6.54E-05	6.51E-05	3.33E-07		3.33E-07		6.51E-05	6.51E-05		
BI+3	7.91E-11	7.87E-11	4.03E-13		4.03E-13		7.87E-11	7.87E-11		
C-14	1.69E-13	1.68E-13	8.57E-16		8.57E-16		1.68E-13	1.68E-13		
CA+2	6.55E-02	6.52E-02	3.33E-04		3.33E-04		6.52E-02	6.52E-02		
CD+2	5.74E-01	5.71E-01	2.92E-03		2.92E-03		5.71E-01	5.71E-01		
CL-	1.74E+04	1.73E+04	8.83E+01		8.83E+01		1.73E+04	1.73E+04		
CL2										
CO2										
CO3-2	4.47E+04	4.44E+04	2.27E+02		2.27E+02		4.44E+04	4.44E+04		
CR(OH)4-	3.13E+03	3.11E+03	1.59E+01		1.59E+01		3.11E+03	3.11E+03		
CS+	1.17E+01	1.16E+01	5.93E-02		5.93E-02		1.16E+01	1.16E+01		
CI+2	5.28E-12	5.25E-12	2.69E-14		2.69E-14		5.25E-12	5.25E-12		
F-	2.23E+02	2.22E+02	1.13E+00		1.13E+00		2.22E+02	2.22E+02		
F2										
FE+3	2.33E+01	2.32E+01	1.19E-01		1.19E-01		2.32E+01	2.32E+01		
H2O	3.03E+06	3.02E+06	1.54E+04	4.02E+05	4.18E+05		3.02E+06	3.02E+06		
K+	1.24E+04	1.24E+04	6.33E+01		6.33E+01		1.24E+04	1.24E+04		
Mg+2	7.99E-02	7.93E-02	4.07E-04		4.07E-04		7.93E-02	7.93E-02		
MN+4	3.40E+00	3.39E+00	1.73E-02		1.73E-02		3.39E+00	3.39E+00		
NH+6	3.53E-02	3.51E-02	1.79E-04		1.79E-04		3.51E-02	3.51E-02		
NO-	5.59E+05	5.56E+05	2.84E+03		2.84E+03		5.56E+05	5.56E+05		
NI+3	3.95E-02	3.93E-02	2.01E-04		2.01E-04		3.93E-02	3.93E-02		
NO2										
NO2-	2.43E+05	2.42E+05	1.24E+03		1.24E+03		2.42E+05	2.42E+05		
NO3-	3.92E+05	3.90E+05	2.00E+03		2.00E+03		3.90E+05	3.90E+05		
NO+4	7.53E-08	7.49E-08	3.83E-10		3.83E-10		7.49E-08	7.49E-08		
O2										
OH-	1.25E+05	1.25E+05	6.37E+02		6.37E+02		1.25E+05	1.25E+05		
FB+4	1.05E-10	1.03E-10	5.36E-13		5.36E-13		1.03E-10	1.03E-10		
FC+3	3.97E+03	3.92E+03	2.02E+01		2.02E+01		3.92E+03	3.92E+03		
FU+4	2.87E-01	2.86E-01	1.46E-03		1.46E-03		2.86E-01	2.86E-01		
SI+4	9.94E-06	9.89E-06	5.05E-08		5.05E-08		9.89E-06	9.89E-06		
SN+4	1.32E-10	1.32E-10	6.72E-13		6.72E-13		1.32E-10	1.32E-10		
SO4-2	1.33E+04	1.32E+04	6.77E+01		6.77E+01		1.32E+04	1.32E+04		
SR+2	4.66E-02	4.63E-02	2.37E-04		2.37E-04		4.63E-02	4.63E-02		
TDO4-	2.54E+01	2.53E+01	1.29E-01		1.29E-01		2.53E+01	2.53E+01		
TI+4	2.64E-12	2.63E-12	1.35E-14		1.35E-14		2.63E-12	2.63E-12		
TCC	7.98E+03	7.93E+03	4.06E+01		4.06E+01		7.93E+03	7.93E+03		
UCO+2	5.90E-01	5.87E-01	3.00E-03		3.00E-03		5.87E-01	5.87E-01		
ZN+2	2.84E+05	2.83E+05	1.43E-07		1.43E-07		2.83E+05	2.83E+05		
ZR+4	1.32E-10	1.32E-10	6.72E-13		6.72E-13		1.32E-10	1.32E-10		

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Table B-13 Phase 1 LAW Mass Balance for Batch PC2/13 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.79E+04	4.79E+02	4.74E+04		4.74E+04		4.79E+02	4.79E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
BE2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
FE2O3										
FORMER										
D2WAT										
K2O										
NaO										
NaNO2										
NaCO3										
Na2O										
NI2O3										
NI2O2										
EGOS										
FR02										
FRU2										
STO2										
SN02										
SiO3										
SOLIDS	4.79E+04	4.79E+02	4.74E+04		4.74E+04		4.79E+02	4.79E+02		
SrO										
TC2O7										
TiO2										
UC6										
ZnO										
ZrO2										

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Table B-13 Phase 1 LAW Mass Balance for Batch PC2/L3 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.35E+06	2.93E+03		2.93E+03	3.35E+06	4.81E+06		1.00E-09	1.00E-09
Density (g/L)		1.42E+03	3.33E+03		3.33E+03	1.42E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.77E+06	9.74E+03		9.74E+03	4.77E+06	4.81E+06		1.00E-09	1.00E-09
RADIONUCLIDES (Ci)										
Cesium		4.26E+03	1.00E+06		1.00E+06	4.26E+03				
Strontium		6.44E+03				6.44E+03				
Technetium		2.38E+02	2.62E+00		2.62E+00	2.58E+02				
TU		2.37E+01				2.37E+01				
CHEMICALS (kg)										
ACH		2.63E-12				2.63E-12				
AL(OH)4-		3.33E+05				3.33E+05				
AM3		8.77E-04				8.77E-04				
AS+5		2.63E-13				2.63E-13				
BH3		8.27E-07				8.27E-07				
BA+2		1.57E-02				1.57E-02				
BE+2		6.51E-05				6.51E-05				
BI+3		7.87E-11				7.87E-11				
C-14		1.68E-13				1.68E-13				
CA+2		6.52E-02				6.52E-02				
CD+2		5.71E-01				5.71E-01				
CL-		1.73E+04				1.73E+04				
CL2							1.73E+04			
CO2							6.17E+04			
CO3-2		4.44E+04				4.44E+04				
CR(OH)4-		3.11E+03				3.11E+03				
CSH		4.92E-02	1.16E+01		1.16E+01	4.92E-02				
CU+2		5.25E-12				5.25E-12				
F-		2.22E+02				2.22E+02		2.22E+02		
F2										
FE+3		2.32E+01				2.32E+01				
H2O		3.02E+06				3.02E+06	3.21E+06		1.00E-09	1.00E-09
K+		1.24E+04				1.24E+04				
MH2		7.95E-02				7.95E-02				
MN+4		3.39E+00				3.39E+00				
MO+6		3.51E-02				3.51E-02				
NA+		5.56E+05	5.59E+03		5.59E+03	5.56E+05				
NH+3		3.93E-02				3.93E-02				
NO2							5.31E+05			
NO2-		2.42E+05				2.42E+05				
NO3-		3.90E+05				3.90E+05				
NI+4		7.49E-08				7.49E-08				
O2							9.85E+05			
OH-		1.25E+05	4.14E+03		4.14E+03	1.25E+05				
OH+4		1.05E-10				1.05E-10				
FO4-3		3.95E+03				3.95E+03				
FU+4		2.86E-01				2.86E-01				
SI+4		9.89E-06				9.89E-06				
SN+4		1.32E-10				1.32E-10				
SO4-2		1.32E+04				1.32E+04				
SR+2		4.63E-02				4.63E-02				
TCD4-		2.50E+01	2.54E-01		2.54E-01	2.50E+01				
TI+4		2.63E-12				2.63E-12				
TCC		7.93E+03				7.93E+03				
UO2+2		5.87E-01				5.87E-01				
ZN+2		2.83E-05				2.83E-05				
ZR+4		1.32E-10				1.32E-10				

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Table B-13 Phase 1 LAW Mass Balance for Batch PC2/L3 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.79E+02		5.59E+03	5.59E+03	4.79E+02	9.60E+05			
RADIOISOTOPES (Ci)										
Cesium							4.26E+03			
Strontium							6.44E+03			
Technetium							2.58E+02			
TU							2.35E+01			
CHEMICALS (kg)										
AC2O							2.83E-12			
AL2O3							1.79E+05			
AM2O3							9.64E-04			
AS2O3							4.04E-13			
B2O3							2.66E-06			
BAO							1.76E-02			
BBO							1.81E-04			
BL2O3							8.78E-11			
CAO							9.12E-02			
ClO							6.32E-01			
CR2O3							1.97E+03			
CS2O							5.21E-02			
CUD							6.58E-12			
FE2O3							3.32E+01			
FURMER										
DMAT				5.59E+03	5.59E+03					
K2O							1.49E+04			
MGO							1.32E-01			
MND2							5.36E+00			
NCO3							5.26E-02			
NK2O							7.50E+05			
NIL2O3							5.53E-02			
NIC2							8.50E-08			
P2O5							2.96E+03			
PBO2							1.21E-10			
PUC2							3.24E-01			
SIC2							2.12E-05			
SN2							1.67E-10			
SO3							1.10E+04			
SOLIDS		4.79E+02					4.79E+02			
SIO							5.46E-02			
TC2O7							2.38E+01			
TIC2							4.39E-12			
UC3							6.22E-01			
ZNO							3.52E-05			
ZRO2							1.78E-10			

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Table B-13 Phase 1 LAW Mass Balance for Batch FC2/L3 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.81E+06				1.60E+06	3.21E+06	2.92E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	4.81E+06				1.60E+06	3.21E+06	9.73E+03	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AP+3									
AS+5									
BH+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	1.73E+04				1.73E+04				
CO2	6.17E+04				6.17E+04				
CO3-2									
CR(OH)4-									
CS+									
CU+2									
F-									
F2	2.22E+02				2.22E+02				
FE+3									
H2O	3.21E+06					3.21E+06			
K+									
MO+2									
MP+4									
MO+6									
NI+							5.59E+03	5.75E-10	
NI+3									
NO2	5.31E+05				5.31E+05				
NO2-									
NO3-									
NI+4									
O2	9.85E+05				9.85E+05				1.00E+06
OH-							4.14E+03	4.25E-10	
EB+4									
EO+3									
EU+4									
SI+4									
SN+4									
SD+2									
SR+2									
TCD4-									
TI+4									
TIC									
UCO+2									
ZN+2									
ZR+4									

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Table B-13 Phase 1 LAW Mass Balance for Batch PC2/13 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		9.60E+05	3.48E+06	4.44E+06					
RADIONUCLIDES (Ci)									
Cesium		4.26E+03		4.26E+03					
Strontium		6.44E+03		6.44E+03					
Technetium		2.58E+02		2.58E+02					
TRU		2.33E+01		2.33E+01					
CHEMICALS (kg)									
AC2O		2.83E-12		2.83E-12					
AL2O3		1.79E+05		1.79E+05					
AM2O3		9.64E-04		9.64E-04					
AS2O3		4.04E-13		4.04E-13					
EGO3		2.66E-06		2.66E-06					
EAO		1.76E-02		1.76E-02					
EBO		1.61E-04		1.61E-04					
ELZOO		8.78E-11		8.78E-11					
CAO		9.12E-02		9.12E-02					
CIO		6.52E-01		6.52E-01					
CR2O3		1.97E+03		1.97E+03					
CS2O		5.21E-02		5.21E-02					
CUO		6.38E-12		6.38E-12					
FE2O3		3.32E+01		3.32E+01					
FORMER			3.48E+06	3.48E+06					
DMPT									
K2O		1.49E+04		1.49E+04					
MGO		1.32E-01		1.32E-01					
MNO2		5.36E+00		5.36E+00					
MCO8		5.26E-02		5.26E-02					
NA2O		7.50E+05		7.50E+05					
NI2O3		5.53E-02		5.53E-02					
NEO2		8.50E-08		8.50E-08					
EGO5		2.96E+03		2.96E+03					
PRO2		1.21E-10		1.21E-10					
FUO2		3.24E-01		3.24E-01					
SIO2		2.12E-05		2.12E-05					
SNO2		1.67E-10		1.67E-10					
SO3		1.10E+04		1.10E+04					
SULFIDS		4.79E+02		4.79E+02					
SRO		5.46E-02		5.46E-02					
TC2O7		2.38E+01		2.38E+01					
TIO2		4.39E-12		4.39E-12					
UC6		6.22E-01		6.22E-01					
ZNO		3.52E-05		3.52E-05					
ZRO2		1.78E-10		1.78E-10					

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Table B-14 Phase 1 LAW Mass Balance for Batch PC2/14 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.81E+06	3.79E+06	1.99E+04	4.49E+05	4.69E+05		3.79E+06	3.79E+06		
Density (g/L)	1.41E+03	1.41E+03	1.41E+03	1.00E+03	1.02E+03		1.41E+03	1.41E+03		
Total Mass Flow (kg)	5.35E+06	5.32E+06	2.79E+04	4.49E+05	4.77E+05		5.32E+06	5.32E+06		
RADIONUCLIDES (Cl)										
Cesium	5.99E+04	5.96E+04	3.13E+02		3.13E+02		5.96E+04	5.96E+04		
Strontium	6.05E+03	6.02E+03	3.16E+01		3.16E+01		6.02E+03	6.02E+03		
Technetium	2.40E+01	2.39E+01	1.25E-01		1.25E-01		2.39E+01	2.39E+01		
Iru	2.52E+00	2.51E+00	1.32E-02		1.32E-02		2.51E+00	2.51E+00		
CHEMICALS (kg)										
AG+	1.61E-01	1.60E-01	8.38E-04		8.38E-04		1.60E-01	1.60E-01		
AL(OH) ₃	2.92E+05	2.91E+05	1.52E+03		1.52E+03		2.91E+05	2.91E+05		
AM#3	3.02E-04	3.01E-04	1.58E-06		1.58E-06		3.01E-04	3.01E-04		
AS#5	9.25E-02	9.20E-02	4.82E-04		4.82E-04		9.20E-02	9.20E-02		
BE#3	4.68E+00	4.66E+00	2.44E-02		2.44E-02		4.66E+00	4.66E+00		
BE#2	3.09E-01	3.08E-01	1.61E-03		1.61E-03		3.08E-01	3.08E-01		
BE#2	2.07E-02	2.05E-02	1.08E-04		1.08E-04		2.05E-02	2.05E-02		
BE#3	7.81E-05	7.77E-05	4.07E-07		4.07E-07		7.77E-05	7.77E-05		
C-14	8.90E-07	8.85E-07	4.64E-09		4.64E-09		8.85E-07	8.85E-07		
CA#2	2.96E+01	2.95E+01	1.55E-01		1.55E-01		2.95E+01	2.95E+01		
CD#2	1.24E-01	1.24E-01	6.49E-04		6.49E-04		1.24E-01	1.24E-01		
CL-	2.99E+04	2.97E+04	1.56E+02		1.56E+02		2.97E+04	2.97E+04		
CL2										
CO2										
CO3-2	7.94E+04	7.90E+04	4.14E+02		4.14E+02		7.90E+04	7.90E+04		
CR(OH) ₃	2.39E+02	2.37E+02	1.24E+00		1.24E+00		2.37E+02	2.37E+02		
CS#	6.92E-01	6.89E-01	3.61E-03		3.61E-03		6.89E-01	6.89E-01		
CH2	5.20E-06	5.17E-06	2.71E-08		2.71E-08		5.17E-06	5.17E-06		
EU-15#	7.94E-10	7.90E-10	4.14E-12		4.14E-12		7.90E-10	7.90E-10		
F-	2.68E+04	2.66E+04	1.40E+02		1.40E+02		2.66E+04	2.66E+04		
F2										
FE#3	1.86E+01	1.85E+01	9.69E-02	4.49E+05	9.69E-02		1.85E+01	1.85E+01		
HO2	3.41E+06	3.40E+06	1.78E+04		4.66E+05		3.40E+06	3.40E+06		
HE#2	3.47E-04	3.46E-04	1.81E-06		1.81E-06		3.46E-04	3.46E-04		
K+	8.45E+03	8.41E+03	4.41E+01		4.41E+01		8.41E+03	8.41E+03		
LA#3	1.82E+00	1.81E+00	9.51E-03		9.51E-03		1.81E+00	1.81E+00		
MF#2	2.62E+01	2.60E+01	1.37E-01		1.37E-01		2.60E+01	2.60E+01		
NN#4	8.10E+01	8.06E+01	4.23E-01		4.23E-01		8.06E+01	8.06E+01		
ND#6	1.12E+01	1.11E+01	5.81E-02		5.81E-02		1.11E+01	1.11E+01		
NA+	6.09E+05	6.06E+05	3.18E+03		3.18E+03		6.06E+05	6.06E+05		
NI#3	1.95E+00	1.94E+00	1.02E-02		1.02E-02		1.94E+00	1.94E+00		
NO2										
NO2-	2.28E+05	2.27E+05	1.19E+03		1.19E+03		2.27E+05	2.27E+05		
NO3-	4.71E+05	4.68E+05	2.46E+03		2.46E+03		4.68E+05	4.68E+05		
NE#4	6.50E-03	6.46E-03	3.39E-05		3.39E-05		6.46E-03	6.46E-03		
O2										
OH-	1.46E+05	1.47E+05	7.71E+02		7.71E+02		1.47E+05	1.47E+05		
FE#4	5.66E-02	5.63E-02	2.95E-04		2.95E-04		5.63E-02	5.63E-02		
FO#-3	1.24E+04	1.23E+04	6.44E+01		6.44E+01		1.23E+04	1.23E+04		
FI#4	2.04E-02	2.03E-02	1.07E-04		1.07E-04		2.03E-02	2.03E-02		
SE#6	1.12E-03	1.12E-03	5.86E-06		5.86E-06		1.12E-03	1.12E-03		
SI#4	5.74E+01	5.71E+01	2.99E-01		2.99E-01		5.71E+01	5.71E+01		
SN#4	1.31E-04	1.30E-04	6.80E-07		6.80E-07		1.30E-04	1.30E-04		
SO#-2	1.68E+04	1.67E+04	8.74E+01		8.74E+01		1.67E+04	1.67E+04		
SR#2	4.36E-02	4.33E-02	2.27E-04		2.27E-04		4.33E-02	4.33E-02		
TDO#	2.32E+00	2.31E+00	1.21E-02		1.21E-02		2.31E+00	2.31E+00		
TI#4	2.61E-06	2.60E-06	1.36E-08		1.36E-08		2.60E-06	2.60E-06		
TCC	1.41E+04	1.40E+04	7.35E+01		7.35E+01		1.40E+04	1.40E+04		
UD#2	1.78E+01	1.77E+01	9.30E-02		9.30E-02		1.77E+01	1.77E+01		
ZN#2	4.20E+00	4.18E+00	2.19E-02		2.19E-02		4.18E+00	4.18E+00		
ZR#4	1.31E-04	1.30E-04	6.80E-07		6.80E-07		1.30E-04	1.30E-04		

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Table B-14 Phase 1 LAW Mass Balance for Batch PC2/14 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	5.35E+04	5.35E+02	5.30E+04		5.30E+04		5.35E+02	5.35E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TiU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
BAO3										
BAO										
BB										
BL2O3										
CAO										
CO										
CR2O3										
CS2O										
CUD										
EU2O3										
FE2O3										
FORMER										
H2O										
IMMAT										
NO										
LA2O3										
NO										
MCO2										
MCO3										
NA2O										
NIL2O3										
NIL2O3										
NICO2										
PO2										
PO2										
PO2										
SE2O										
SIO2										
SNCO2										
SO3										
SOLIDS	5.35E+04	5.35E+02	5.30E+04		5.30E+04		5.35E+02	5.35E+02		
SRO										
TC2O7										
TIO2										
UC3										
ZNO										
ZNCO2										

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Table B-14 Phase 1 LAW Mass Balance for Batch PC2/14 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.79E+06	3.18E+03		3.18E+03	3.79E+06	5.32E+06		1.00E-09	1.00E-09
Density (g/L)		1.41E+03	3.34E+03		3.34E+03	1.41E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		5.32E+06	1.06E+04		1.06E+04	5.32E+06	5.32E+06		1.00E-09	1.00E-09
RADIONUCLIDES (Ci)										
Cesium		4.63E+03	5.50E+04		5.50E+04	4.63E+03				
Strontium		6.02E+03				6.02E+03				
Technetium		2.36E+01	2.40E-01		2.40E-01	2.36E+01				
TRI		2.51E+00				2.51E+00				
CHEMICALS (kg)										
AG+		1.60E-01				1.60E-01				
AL(OH) ₄ -		2.91E+05				2.91E+05				
AM+3		3.01E-04				3.01E-04				
AS+5		9.20E-02				9.20E-02				
BS+3		4.66E+00				4.66E+00				
BS+2		3.09E-01				3.09E-01				
BE+2		2.05E-02				2.05E-02				
BI+3		7.77E-05				7.77E-05				
C-14		8.85E-07				8.85E-07				
CA+2		2.95E+01				2.95E+01				
CD+2		1.24E-01				1.24E-01				
CL-		2.97E+04				2.97E+04				
CL2							2.97E+04			
CO2							1.09E+05			
CO3-2		7.90E+04				7.90E+04				
CR(OH) ₄ -		2.37E+02				2.37E+02				
CS+		5.37E-02	6.35E-01		6.35E-01	5.37E-02				
ClH2		5.17E-06				5.17E-06				
EJ-154		7.90E-10				7.90E-10				
F-		2.66E+04				2.66E+04				
F2							2.66E+04			
FE+3		1.85E+01				1.85E+01				
H2O		3.40E+06				3.40E+06		1.00E-09		1.00E-09
HE+2		3.46E-04				3.46E-04				
HP+		8.41E+03				8.41E+03				
IA+3		1.81E+00				1.81E+00				
MD+2		2.60E+01				2.60E+01				
MN+4		8.06E+01				8.06E+01				
ND+6		1.11E+01				1.11E+01				
NA+		6.06E+05	6.09E+03		6.09E+03	6.06E+05				
NI+3		1.94E+00				1.94E+00				
NO2							5.75E+05			
NO2-		2.27E+05				2.27E+05				
NO3-		4.68E+05				4.68E+05				
NE+4		6.46E-03				6.46E-03				
O2							9.91E+05			
OH-		1.47E+05	4.51E+03		4.51E+03	1.47E+05				
FB+4		5.63E-02				5.63E-02				
FO4-3		1.23E+04				1.23E+04				
FU+4		2.03E-02				2.03E-02				
SE+6		1.12E-03				1.12E-03				
SI+4		5.71E+01				5.71E+01				
SN+4		1.30E-04				1.30E-04				
SO4-2		1.67E+04				1.67E+04				
SR+2		4.33E-02				4.33E-02				
TU4-		2.29E+00				2.29E+00				
TI+4		2.60E-06				2.60E-06				
IO3		1.40E+04				1.40E+04				
UO2+2		1.77E+01				1.77E+01				
ZN+2		4.18E+00				4.18E+00				
ZR+4		1.30E-04				1.30E-04				

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Table B-14 Phase 1 LAW Mass Balance for Batch PC2/14 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		5.35E+02		6.09E+03	6.09E+03	5.35E+02	1.01E+06			
RADIONUCLIDES (Cl)										
Cesium							4.65E+03			
Strontium							6.02E+03			
Technetium							2.36E+01			
TU1							2.49E+00			
CHEMICALS (kg)										
AC2O							1.72E-01			
AL2O3							1.56E+05			
AM2O3							3.31E-04			
AS2O5							1.41E-01			
B2O3							1.50E+01			
BAO							3.44E-01			
BBO							5.70E-02			
BL2O3							8.66E-05			
CAO							4.13E+01			
ClO							1.41E-01			
CR2O3							1.50E+02			
CS2O							5.68E-02			
CUO							6.48E-06			
EU2O3							9.15E-10			
FE2O3							2.64E+01			
FORMER										
H2O							3.73E-04			
DMAC										
K2O							1.01E+04			
LA2O3							2.13E+00			
MO							4.32E+01			
MNO2							1.28E+02			
MCO3							1.66E+01			
NA2O							8.17E+05			
NI2O3							2.74E+00			
NICO2							7.34E-03			
PO5							9.19E+03			
PHO2							6.50E-02			
PUC2							2.30E-02			
SECO							1.80E-03			
SICO2							1.22E+02			
SNO2							1.65E-04			
SO3							1.39E+04			
SOLIDS		5.35E+02				5.35E+02	5.35E+02			
SFO							5.10E-02			
TC2O7							2.18E+00			
TICO2							4.33E-06			
UCO							1.88E+01			
ZNO							5.20E+00			
ZRO2							1.75E-04			

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Table B-14 Phase 1 LAW Mass Balance for Batch PC2/14 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	5.32E+06				1.73E+06	3.58E+06	3.18E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	5.32E+06				1.73E+06	3.58E+06	1.06E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AGP									
AL(OH)4-									
AN#3									
ASH5									
B#3									
BA#2									
BE#2									
BI#3									
C-14									
CA#2									
CD#2									
CL-									
CL2	2.97E+04				2.97E+04				
CO2	1.09E+05				1.09E+05				
CO3-2									
CR(OH)4-									
CS+									
CH2									
EI-154									
F-									
F2	2.66E+04				2.66E+04				
FE#3	3.58E+06					3.58E+06			
H2O									
HG#2									
K+									
LA#3									
ME#2									
MA#4									
MD#6									
NA+							6.09E+03	5.75E-10	
NI#3									
NO2	5.75E+05				5.75E+05				
NO2-									
NO3-									
NE#4									
O2	9.91E+05				9.91E+05				1.00E+06
OH-									
EB#4							4.51E+03	4.25E-10	
EO#-3									
EU#4									
SE#6									
SI#4									
SN#4									
SD#-2									
SR#2									
TCD#4									
TI#4									
TCC									
UD#12									
ZN#2									
ZR#4									

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Table B-14 Phase 1 LAW Mass Balance for Batch PC2/14 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		1.01E+06	3.83E+06	4.84E+06					
RADIONUCLIDES (Cl)									
Cesium		4.65E+03		4.65E+03					
Strontium		6.02E+03		6.02E+03					
Technetium		2.36E+01		2.36E+01					
TU		2.49E+00		2.49E+00					
CHEMICALS (kg)									
AG30		1.72E-01		1.72E-01					
AL2O3		1.56E+05		1.56E+05					
AM2O5		3.31E-04		3.31E-04					
AS2O5		1.41E-01		1.41E-01					
B2O3		1.50E+01		1.50E+01					
B4O		3.44E-01		3.44E-01					
BBO		5.70E-02		5.70E-02					
Bi2O3		8.66E-05		8.66E-05					
CaO		4.13E+01		4.13E+01					
CaO		1.41E-01		1.41E-01					
CR2O3		1.50E+02		1.50E+02					
CS2O		5.68E-02		5.68E-02					
CUO		6.48E-06		6.48E-06					
EU2O3		9.15E-10		9.15E-10					
FE2O3		2.64E+01		2.64E+01					
FORMER			3.83E+06		3.83E+06				
HEO		3.73E-04		3.73E-04					
HMAT									
K2O		1.01E+04		1.01E+04					
LAGO3		2.13E+00		2.13E+00					
MO		4.32E+01		4.32E+01					
MNO2		1.28E+02		1.28E+02					
MCO3		1.66E+01		1.66E+01					
NA2O		8.17E+05		8.17E+05					
NI2O3		2.74E+00		2.74E+00					
NEO2		7.34E-03		7.34E-03					
P2O5		9.19E+03		9.19E+03					
PBO2		6.50E-02		6.50E-02					
PLU2		2.30E-02		2.30E-02					
SEO3		1.80E-03		1.80E-03					
STO2		1.22E+02		1.22E+02					
SNO2		1.65E-04		1.65E-04					
SO6		1.39E+04		1.39E+04					
SOLIDS		5.35E+02		5.35E+02					
SRO		5.10E-02		5.10E-02					
TC2O7		2.18E+00		2.18E+00					
TIO2		4.33E-06		4.33E-06					
UO3		1.88E+01		1.88E+01					
ZNO		5.20E+00		5.20E+00					
ZRO2		1.75E-04		1.75E-04					

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Table B-15 Phase 1 LAW Mass Balance for Batch PC2/15 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	2.38E+06	2.37E+06	1.16E+04	2.80E+05	2.92E+05		2.37E+06	2.37E+06		
Density (g/L)	1.40E+03	1.40E+03	1.40E+03	1.00E+03	1.02E+03		1.40E+03	1.40E+03		
Total Mass Flow (kg)	3.33E+06	3.31E+06	1.62E+04	2.80E+05	2.96E+05		3.31E+06	3.31E+06		
RADIONUCLIDES (Ci)										
Cesium	1.04E+06	1.04E+06	5.06E+03		5.06E+03		1.04E+06	1.04E+06		
Strontium	1.38E+04	1.37E+04	6.72E+01		6.72E+01		1.37E+04	1.37E+04		
Technetium	1.80E+02	1.79E+02	8.77E-01		8.77E-01		1.79E+02	1.79E+02		
I-131	1.65E+01	1.64E+01	8.00E-02		8.00E-02		1.64E+01	1.64E+01		
CHEMICALS (kg)										
AG+	7.50E-03	7.46E-03	3.63E-05		3.63E-05		7.46E-03	7.46E-03		
AL(OH)4-	1.94E+05	1.94E+05	9.46E+02		9.46E+02		1.94E+05	1.94E+05		
AM+3	6.19E-04	6.16E-04	3.01E-06		3.01E-06		6.16E-04	6.16E-04		
AM+5	4.32E-03	4.30E-03	2.10E-05		2.10E-05		4.30E-03	4.30E-03		
BP+3	2.19E-01	2.18E-01	1.05E-03		1.05E-03		2.18E-01	2.18E-01		
BP+2	1.44E-02	1.42E-02	7.92E-05		7.92E-05		1.44E-02	1.44E-02		
BE+2	9.68E-04	9.63E-04	4.71E-06		4.71E-06		9.63E-04	9.63E-04		
BI+3	3.63E-06	3.63E-06	1.77E-08		1.77E-08		3.63E-06	3.63E-06		
C-14	4.15E-08	4.13E-08	2.02E-10		2.02E-10		4.13E-08	4.13E-08		
CA+2	1.38E+00	1.38E+00	6.73E-03		6.73E-03		1.38E+00	1.38E+00		
CD+2	5.46E-03	5.43E-03	2.66E-05		2.66E-05		5.43E-03	5.43E-03		
CL-	1.17E+04	1.16E+04	5.68E+01		5.68E+01		1.16E+04	1.16E+04		
CL2										
CO2										
CO3-2	4.23E+04	4.23E+04	2.07E+02		2.07E+02		4.23E+04	4.23E+04		
CR(OH)4-	2.13E+03	2.12E+03	1.03E+01		1.03E+01		2.12E+03	2.12E+03		
CS-	1.20E+01	1.20E+01	5.84E-02		5.84E-02		1.20E+01	1.20E+01		
CH2	2.43E-07	2.42E-07	1.18E-09		1.18E-09		2.42E-07	2.42E-07		
EU-154	3.71E-11	3.69E-11	1.80E-13		1.80E-13		3.69E-11	3.69E-11		
F-	1.25E+03	1.25E+03	6.10E+00		6.10E+00		1.25E+03	1.25E+03		
F2										
FE+3	1.62E+01	1.61E+01	7.86E-02	2.80E+05	7.86E-02		1.61E+01	1.61E+01		
H2O	2.12E+06	2.11E+06	1.03E+04		2.91E+05		2.11E+06	2.11E+06		
H2O2	1.62E-05	1.62E-05	7.90E-08		7.90E-08		1.62E-05	1.62E-05		
K+	1.02E+04	1.02E+04	4.96E+01		4.96E+01		1.02E+04	1.02E+04		
LA+3	8.52E-02	8.48E-02	4.13E-04		4.13E-04		8.48E-02	8.48E-02		
MO+2	1.22E+00	1.21E+00	5.93E-03		5.93E-03		1.21E+00	1.21E+00		
MN+4	3.78E+00	3.77E+00	1.84E-02		1.84E-02		3.77E+00	3.77E+00		
MO+6	5.22E-01	5.19E-01	2.54E-03		2.54E-03		5.19E-01	5.19E-01		
Na+	4.06E+05	4.04E+05	1.98E+03		1.98E+03		4.04E+05	4.04E+05		
NI+3	9.07E-02	9.03E-02	4.41E-04		4.41E-04		9.03E-02	9.03E-02		
NO2										
NO2-	1.31E+05	1.31E+05	6.39E+02		6.39E+02		1.31E+05	1.31E+05		
NO3-	2.85E+05	2.84E+05	1.39E+03		1.39E+03		2.84E+05	2.84E+05		
NE+4	3.03E-04	3.02E-04	1.48E-06		1.48E-06		3.02E-04	3.02E-04		
O2										
OH-	1.02E+05	1.02E+05	4.96E+02		4.96E+02		1.02E+05	1.02E+05		
PH4	2.64E+03	2.63E+03	1.29E-05		1.29E-05		2.63E+03	2.63E+03		
PO4-3	4.40E+03	4.38E+03	2.14E+01		2.14E+01		4.38E+03	4.38E+03		
PU+4	1.98E-01	1.97E-01	9.62E-04		9.62E-04		1.97E-01	1.97E-01		
SE+6	5.25E-05	5.23E-05	2.56E-07		2.56E-07		5.23E-05	5.23E-05		
SI+4	2.68E+00	2.67E+00	1.30E-02		1.30E-02		2.67E+00	2.67E+00		
SN+4	6.07E-06	6.04E-06	2.96E-08		2.96E-08		6.04E-06	6.04E-06		
SD4-2	9.76E+03	9.72E+03	4.73E+01		4.73E+01		9.72E+03	9.72E+03		
SH+2	9.94E-02	9.89E-02	4.84E-04		4.84E-04		9.89E-02	9.89E-02		
TD4-	1.75E+01	1.74E+01	8.49E-02		8.49E-02		1.74E+01	1.74E+01		
TI+4	1.22E-07	1.21E-07	5.93E-10		5.93E-10		1.21E-07	1.21E-07		
TIC	4.97E+03	4.94E+03	3.39E+01		3.39E+01		4.94E+03	4.94E+03		
UCO+2	8.34E-01	8.30E-01	4.06E-03		4.06E-03		8.30E-01	8.30E-01		
ZN+2	1.96E-01	1.95E-01	9.54E-04		9.54E-04		1.95E-01	1.95E-01		
ZR+4	6.07E-06	6.04E-06	2.96E-08		2.96E-08		6.04E-06	6.04E-06		

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Table B-15 Phase 1 LAW Mass Balance for Batch PC2/15 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.33E+04	3.33E+02	3.29E+04		3.29E+04		3.33E+02	3.33E+02		
RADIONUCLIDES (Cl)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
EG2O										
BAO										
BD										
BL2O3										
CAO										
ClO										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
H2O										
DMAT										
K2O										
LA2O3										
MO										
MO2										
MO3										
NA2O										
NIL2O3										
NEO2										
EG25										
FKO2										
FLU2										
SEO3										
SI1O2										
SN2O2										
SO3										
SOLIDS	3.33E+04	3.33E+02	3.29E+04		3.29E+04		3.33E+02	3.33E+02		
SO										
TC2O7										
TIC2										
U3										
ZNO										
ZRC2										

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Table B-15 Phase 1 LAW Mass Balance for Batch PC2/L5 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		2.37E+06	2.13E+03		2.13E+03	2.37E+06	3.64E+06		1.00E-09	1.00E-09
Density (g/L)		1.40E+03	3.32E+03		3.32E+03	1.40E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		3.31E+06	7.08E+03		7.08E+03	3.31E+06	3.64E+06		1.00E-09	1.00E-09

RADIONUCLIDES (Ci)										
Cesium		3.10E+03	1.03E+06		1.03E+06	3.10E+03				
Strontium		1.37E+04				1.37E+04				
Technetium		1.78E+02	1.80E+00		1.80E+00	1.78E+02				
TU1		1.64E+01				1.64E+01				

CHEMICALS (kg)										
AG+		7.46E-03				7.46E-03				
AL(OH)4-		1.94E+05				1.94E+05				
AM+3		6.16E-04				6.16E-04				
AS+5		4.30E-03				4.30E-03				
BA+3		2.18E-01				2.18E-01				
BA+2		1.44E-02				1.44E-02				
BE+2		9.63E-04				9.63E-04				
BI+3		3.63E-06				3.63E-06				
C-14		4.13E-08				4.13E-08				
CA+2		1.38E+00				1.38E+00				
CD+2		5.43E-03				5.43E-03				
CL-		1.16E+04				1.16E+04				
CL2									1.16E+04	
CO2									5.63E+04	
CO3-2		4.23E+04				4.23E+04				
CR(OH)4-		2.14E+03				2.14E+03				
CS+		3.58E-02	1.19E+01		1.19E+01	3.58E-02				
ClH2		2.42E-07				2.42E-07				
EJ-154		3.69E-11				3.69E-11				
F-		1.25E+03				1.25E+03				
F2									1.25E+03	
FE+3		1.61E+01				1.61E+01				
H2O		2.11E+06				2.11E+06	2.23E+06		1.00E-09	1.00E-09
HE+2		1.62E-05				1.62E-05				
H+		1.02E+04				1.02E+04				
IA+3		8.48E-02				8.48E-02				
MD+2		1.21E+00				1.21E+00				
MN+4		3.77E+00				3.77E+00				
ND+6		5.19E-01				5.19E-01				
NA+		4.04E+05	4.06E+03		4.06E+03	4.04E+05				
NI+3		9.03E-02				9.03E-02				
NO2									3.41E+05	
NO2-		1.31E+05				1.31E+05				
NO3-		2.84E+05				2.84E+05				
NO3H4		3.02E-04				3.02E-04				
O2									9.90E+05	
OH-		1.02E+05	3.01E+03		3.01E+03	1.02E+05				
OH+4		2.63E-03				2.63E-03				
FO4-3		4.38E+03				4.38E+03				
FU+4		1.97E-01				1.97E-01				
SE+6		5.23E-05				5.23E-05				
SI+4		2.67E+00				2.67E+00				
SH+4		6.04E-06				6.04E-06				
SO4-2		9.72E+03				9.72E+03				
SR+2		9.69E-02				9.69E-02				
TCl3-4		1.72E+01	1.75E-01		1.75E-01	1.72E+01				
TI+4		1.21E-07				1.21E-07				
TU2		6.94E+03				6.94E+03				
UD2+2		8.30E-01				8.30E-01				
ZM+2		1.95E-01				1.95E-01				
Zr+4		6.04E-06				6.04E-06				

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Table B-15 Phase 1 LAW Mass Balance for Batch PC2/15 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		3.33E+02		4.06E+03	4.06E+03	3.33E+02	6.74E+05			
RADIONUCLIDES (Cl)										
Cesium							3.10E+03			
Strontium							1.37E+04			
Technetium							1.78E+02			
TU1							1.62E+01			
CHEMICALS (kg)										
Ag2O							8.02E-03			
Al2O3							1.04E+05			
Am2O3							6.77E-04			
As2O3							6.59E-03			
BaO							7.01E-01			
BaF							1.60E-02			
BaO							2.67E-03			
Bi2O3							4.05E-06			
CaO							1.93E+00			
ClO							6.21E-03			
Cr2O3							1.36E+03			
CS2O							3.79E-02			
CUO							3.02E-07			
EU2O3							4.27E-11			
FE2O3							2.30E+01			
FORMER										
H2O							1.75E-05			
HM2O										
K2O				4.06E+03	4.06E+03		1.22E+04			
La2O3							9.94E-02			
MO							2.01E+00			
MnO2							5.96E+00			
MCO3							7.79E-01			
Na2O							5.45E+05			
Ni2O3							1.27E-01			
NiO2							3.43E-04			
P2O5							3.27E+03			
PrO2							3.04E-03			
RuO2							2.23E-01			
SeO3							8.41E-05			
SiO2							5.70E+00			
SnO2							7.67E-06			
SO3							8.10E+03			
SOLIDS							3.33E+02			
SrO		3.33E+02				3.33E+02	1.17E-01			
Ta2O7							1.64E+01			
TiO2							2.02E-07			
UO3							8.79E-01			
ZnO							2.43E-01			
ZrO2							8.17E-06			

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Table B-15 Phase 1 LAW Mass Balance for Batch PC2/15 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	3.64E+06				1.40E+06	2.23E+06	2.12E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	3.64E+06				1.40E+06	2.23E+06	7.07E+03	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH) ₄ ⁻									
As+3									
As+5									
B+3									
Ba+2									
Be+2									
Bi+3									
C-14									
Ca+2									
CD+2									
Cl-									
Cl ₂	1.16E+04				1.16E+04				
CO ₂	5.65E+04				5.65E+04				
CO ₃ ⁻²									
CR(OH) ₄ ⁻									
CS+									
Cl ₂ H									
EJ-154									
F-									
F ₂	1.25E+03				1.25E+03				
FE+3									
H ₂ O	2.23E+06					2.23E+06			
Hg+2									
K+									
LA+3									
MB+2									
MA+4									
MD+6									
Na+							4.06E+03	5.75E-10	
NI+3									
NO ₂	3.41E+05				3.41E+05				
NO ₂ ⁻									
NO ₃ ⁻									
NE+4									
O ₂	9.90E+05				9.90E+05				1.00E+06
OH-									
EB+4							3.01E+03	4.25E-10	
EO ₄ ⁻³									
EU+4									
SE+6									
SI+4									
SR+4									
SO ₄ ⁻²									
SR+2									
TDO ₄ ⁻									
TI+4									
TiC									
UD ₂ +2									
ZN+2									
ZR+4									

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Table B-15 Phase 1 LAW Mass Balance for Batch PC2/15 (6 sheets)

STREAM NAME SOLID COMPONENTS	20	21	22	23	24	25	26	27	28
Total Mass Flow (kg)		6.74E+05	2.55E+06	3.23E+06					
RADIONUCLIDES (Cl)									
Cesium		3.10E+03		3.10E+03					
Strontium		1.37E+04		1.37E+04					
Technetium		1.78E+02		1.78E+02					
TU		1.62E+01		1.62E+01					
CHEMICALS (kg)									
AC2O		8.02E-03		8.02E-03					
AL2O3		1.04E+05		1.04E+05					
AM2O3		6.77E-04		6.77E-04					
AS2O5		6.59E-03		6.59E-03					
EG2O		7.01E-01		7.01E-01					
EA2O		1.60E-02		1.60E-02					
ED2O		2.67E-03		2.67E-03					
EL2O3		4.05E-06		4.05E-06					
GA2O		1.93E+00		1.93E+00					
GD2O		6.21E-03		6.21E-03					
GR2O3		1.36E+03		1.36E+03					
CS2O		3.79E-02		3.79E-02					
CU2O		3.02E-07		3.02E-07					
EU2O3		4.27E-11		4.27E-11					
FE2O3		2.30E+01	2.55E+06	2.30E+01					
FORMER				2.55E+06					
H2O		1.75E-05		1.75E-05					
IB2O4T									
K2O		1.22E+04		1.22E+04					
LA2O3		9.94E-02		9.94E-02					
ND2O		2.01E+00		2.01E+00					
MN2O2		5.96E+00		5.96E+00					
MO2O		7.79E-01		7.79E-01					
NA2O		5.45E+05		5.45E+05					
NI2O3		1.27E-01		1.27E-01					
NF2O2		3.43E-04		3.43E-04					
PO2O5		3.27E+03		3.27E+03					
PR2O2		3.04E-03		3.04E-03					
PU2O2		2.23E-01		2.23E-01					
SE2O3		8.41E-05		8.41E-05					
SI2O2		5.70E+00		5.70E+00					
SN2O2		7.67E-06		7.67E-06					
SO3		8.10E+03		8.10E+03					
SOLIDS		3.33E+02		3.33E+02					
SRO		1.17E-01		1.17E-01					
TC2O7		1.64E+01		1.64E+01					
TI2O2		2.02E-07		2.02E-07					
UX3		8.79E-01		8.79E-01					
ZNO		2.43E-01		2.43E-01					
ZR2O2		8.17E-06		8.17E-06					

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Table B-16 Phase 1 LAW Mass Balance for Batch PC2/16 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	2.62E+06	2.61E+06	1.33E+04	3.19E+05	3.32E+05		2.61E+06	2.61E+06		
Density (g/L)	1.45E+03	1.45E+03	1.45E+03	1.00E+03	1.02E+03		1.43E+03	1.43E+03		
Total Mass Flow (kg)	3.80E+06	3.78E+06	1.93E+04	3.19E+05	3.38E+05		3.78E+06	3.78E+06		
RADIONUCLIDES (Ci)										
Cesium	9.58E+05	9.53E+05	4.86E+03		4.86E+03		9.53E+05	9.53E+05		
Strontium	3.06E+03	2.99E+03	1.52E+01		1.52E+01		2.99E+03	2.99E+03		
Technetium	2.86E+02	2.94E+02	1.43E+00		1.43E+00		2.84E+02	2.84E+02		
IU1	5.48E+00	5.46E+00	2.78E-02		2.78E-02		5.46E+00	5.46E+00		
CHEMICALS (kg)										
AG+	4.29E-04	4.26E-04	2.17E-06		2.17E-06		4.26E-04	4.26E-04		
AL(OH)4-	1.91E+05	1.90E+05	9.69E+02		9.69E+02		1.90E+05	1.90E+05		
AM+3	6.77E-04	6.73E-04	3.43E-06		3.43E-06		6.73E-04	6.73E-04		
AS+5	2.47E-04	2.46E-04	1.23E-06		1.23E-06		2.46E-04	2.46E-04		
BH+	1.25E-02	1.25E-02	6.34E-05		6.34E-05		1.25E-02	1.25E-02		
BA+2	8.24E-04	8.20E-04	4.18E-06		4.18E-06		8.20E-04	8.20E-04		
BE+2	5.52E-05	5.49E-05	2.80E-07		2.80E-07		5.49E-05	5.49E-05		
BI+3	2.08E-07	2.07E-07	1.06E-09		1.06E-09		2.07E-07	2.07E-07		
C-14	1.49E-04	1.48E-04	7.54E-07		7.54E-07		1.48E-04	1.48E-04		
CA+2	5.96E+01	5.93E+01	3.02E-01		3.02E-01		5.93E+01	5.93E+01		
CD+2	3.03E-04	3.03E-04	1.52E-06		1.52E-06		3.03E-04	3.03E-04		
CL-	1.02E+04	1.01E+04	5.17E+01		5.17E+01		1.01E+04	1.01E+04		
CL2										
CO2										
CO3-2	2.53E+04	2.52E+04	1.28E+02		1.28E+02		2.52E+04	2.52E+04		
CR(OH)4-	8.32E+02	8.28E+02	4.22E+00		4.22E+00		8.28E+02	8.28E+02		
CS+	1.11E+01	1.10E+01	5.61E-02		5.61E-02		1.10E+01	1.10E+01		
CH+2	1.39E-08	1.38E-08	7.06E-11		7.06E-11		1.38E-08	1.38E-08		
EU-154	2.12E-12	2.11E-12	1.07E-14		1.07E-14		2.11E-12	2.11E-12		
F-	7.15E+01	7.12E+01	3.63E-01		3.63E-01		7.12E+01	7.12E+01		
F2										
FE+3	1.22E+00	1.21E+00	6.18E-03	3.19E+05	6.18E-03		1.21E+00	1.21E+00		
H2O	2.27E+06	2.26E+06	1.15E+04		3.30E+05		2.26E+06	2.26E+06		
HO+2	9.23E-07	9.20E-07	4.69E-09		4.69E-09		9.20E-07	9.20E-07		
K+	7.60E+04	7.55E+04	3.83E+02		3.83E+02		7.55E+04	7.55E+04		
LA+3	4.87E-03	4.83E-03	2.47E-05		2.47E-05		4.83E-03	4.83E-03		
MD+2	9.42E+01	9.37E+01	4.78E-01		4.78E-01		9.37E+01	9.37E+01		
MM+4	4.72E+01	4.69E+01	2.39E-01		2.39E-01		4.69E+01	4.69E+01		
MD+6	1.04E+02	1.03E+02	5.26E-01		5.26E-01		1.03E+02	1.03E+02		
NA+	4.44E+05	4.42E+05	2.25E+03		2.25E+03		4.42E+05	4.42E+05		
NI+3	5.20E-03	5.18E-03	2.64E-05		2.64E-05		5.18E-03	5.18E-03		
NO2										
NCL-	1.94E+05	1.93E+05	9.82E+02		9.82E+02		1.93E+05	1.93E+05		
NC3-	4.06E+05	4.04E+05	2.06E+03		2.06E+03		4.04E+05	4.04E+05		
NE+4	1.74E-05	1.73E-05	8.81E-08		8.81E-08		1.73E-05	1.73E-05		
O2										
OH-	1.63E+05	1.63E+05	8.28E+02		8.28E+02		1.63E+05	1.63E+05		
FB+4	5.45E+02	5.42E+02	2.77E+00		2.77E+00		5.42E+02	5.42E+02		
EO4-3	4.12E+03	4.10E+03	2.09E+01		2.09E+01		4.10E+03	4.10E+03		
FU+4	4.36E-02	4.34E-02	2.21E-04		2.21E-04		4.34E-02	4.34E-02		
SE+6	5.93E-02	5.92E-02	3.02E-04		3.02E-04		5.92E-02	5.92E-02		
SI+4	1.53E-01	1.52E-01	7.76E-04		7.76E-04		1.52E-01	1.52E-01		
SM+4	3.47E-07	3.46E-07	1.76E-09		1.76E-09		3.46E-07	3.46E-07		
SO4-2	2.56E+03	2.57E+03	1.31E+01		1.31E+01		2.57E+03	2.57E+03		
SR+2	2.16E-02	2.15E-02	1.10E-04		1.10E-04		2.15E-02	2.15E-02		
TCO4-	2.77E+01	2.75E+01	1.40E-01		1.40E-01		2.75E+01	2.75E+01		
TI+4	8.51E+00	8.47E+00	4.32E-02		4.32E-02		8.47E+00	8.47E+00		
TIC	4.94E+03	4.92E+03	2.51E+01		2.51E+01		4.92E+03	4.92E+03		
UC2+2	8.59E+02	8.55E+02	4.36E+00		4.36E+00		8.55E+02	8.55E+02		
ZN+2	5.69E+02	5.66E+02	2.88E+00		2.88E+00		5.66E+02	5.66E+02		
ZR+4	9.07E+01	9.03E+01	4.60E-01		4.60E-01		9.03E+01	9.03E+01		

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Table B-16 Phase 1 LAW Mass Balance for Batch FC2/16 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.79E+04	3.79E+02	3.76E+04		3.76E+04		3.79E+02	3.79E+02		
RADIONUCLIDES (CL)										
Cesium										
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AS2O										
AL2O3										
AN2O3										
AS2O5										
B2O3										
B4O										
B2O										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
ClO										
EL2O3										
FE2O3										
FORMER										
HEO										
DMFAT										
K2O										
LA2O3										
MO										
MO2										
MO3										
NA2O										
NIL2O3										
NPC2										
PC2O5										
PH2O2										
PL2O2										
SE2O3										
SiO2										
SiO2										
SO3										
SULFUR	3.79E+04	3.79E+02	3.76E+04		3.76E+04		3.79E+02	3.79E+02		
SrO										
TC2O7										
TiO2										
UO3										
ZNO										
ZnO2										

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Table B-16 Phase 1 LAW Mass Balance for Batch PC2/16 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		2.61E+06	2.33E+03		2.33E+03	2.61E+06	3.98E+06		1.00E-09	1.00E-09
Density (g/L)		1.45E+03	3.33E+03		3.33E+03	1.45E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		3.78E+06	7.74E+03		7.74E+03	3.78E+06	3.98E+06		1.00E-09	1.00E-09

RADIONUCLIDES (Ci)										
Cesium		3.39E+03	9.50E+05		9.50E+05	3.39E+03				
Strontium		2.99E+03				2.99E+03				
Technetium		2.81E+02	2.86E+00		2.86E+00	2.81E+02				
IU		5.46E+00				5.46E+00				

CHEMICALS (kg)										
AGP		4.26E-04				4.26E-04				
AL(OH)4-		1.90E+05				1.90E+05				
AM#3		6.73E-04				6.73E-04				
AS#5		2.46E-04				2.46E-04				
BP#3		1.25E-02				1.25E-02				
BA#2		8.20E-04				8.20E-04				
BE#2		5.49E-05				5.49E-05				
BI#3		2.07E-07				2.07E-07				
C-14		1.48E-04				1.48E-04				
CA#2		5.93E+01				5.93E+01				
CD#2		3.03E-04				3.03E-04				
CL-		1.01E+04				1.01E+04				
CL2							1.01E+04			
CO2							3.65E+04			
CO3-2		2.52E+04				2.52E+04				
CR(OH)4-		8.28E+02				8.28E+02				
CS#		3.91E-02	1.10E+01		1.10E+01	3.91E-02				
CU#2		1.38E-08				1.38E-08				
EU-154		2.11E-12				2.11E-12				
F-		7.12E+01				7.12E+01				
F2							7.12E+01			
FE#3		1.21E+00				1.21E+00				
H2O		2.26E+06				2.26E+06	2.42E+06		1.00E-09	1.00E-09
H3#2		9.20E-07				9.20E-07				
H#		7.56E+04				7.56E+04				
IA#3		4.85E-03				4.85E-03				
MD#2		9.37E+01				9.37E+01				
MN#4		4.69E+01				4.69E+01				
ND#6		1.03E+02				1.03E+02				
NA#		4.44E+05	4.44E+03		4.44E+03	4.42E+05				
NI#3		5.18E-03				5.18E-03				
NO2							4.92E+05			
NO2-		1.93E+05				1.93E+05				
NO3-		4.04E+05				4.04E+05				
NH#4		1.73E-05				1.73E-05				
O2							1.02E+06			
OH-		1.63E+05	3.29E+03		3.29E+03	1.63E+05				
FB#4		5.42E+02				5.42E+02				
FO#-3		4.10E+03				4.10E+03				
FU#4		4.34E-02				4.34E-02				
SE#6		5.92E-02				5.92E-02				
SI#4		1.52E-01				1.52E-01				
SM#4		3.46E-07				3.46E-07				
SO#-2		2.57E+03				2.57E+03				
SR#2		2.13E-02				2.13E-02				
TCO#4		2.72E+01				2.72E+01				
TI#4		8.47E+00	2.77E-01		2.77E-01	8.47E+00				
TCC		4.92E+03				4.92E+03				
UD#2		8.55E+02				8.55E+02				
ZN#2		5.66E+02				5.66E+02				
ZR#4		9.03E+01				9.03E+01				

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Table B-16 Phase 1 LAW Mass Balance for Batch PC2/16 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		3.79E+02		4.44E+03	4.44E+03	3.79E+02	7.98E+05			
RADIONUCLIDES (Cl)										
Cesium							3.39E+03			
Strontium							2.99E+03			
Technetium							2.81E+02			
TU							5.42E+00			
CHEMICALS (kg)										
AGG0							4.58E-04			
AL2O3							1.02E+05			
AM2O3							7.40E-04			
AS2O5							3.77E-04			
B2O3							4.01E-02			
BAO							9.16E-04			
BAO							1.32E-04			
BL2O3							2.31E-07			
CAO							8.30E+01			
ClO							3.47E-04			
CR2O3							5.24E+02			
CS2O							4.14E-02			
ClO							1.73E-08			
FL2O3							2.44E-12			
FE2O3							1.73E+00			
FORMER										
H2O							9.93E-07			
IMMAT										
K2O				4.44E+03	4.44E+03		9.10E+04			
LA2O3							5.69E-03			
MO							1.55E+02			
MNO2							7.43E+01			
MO3							1.55E+02			
NA2O							5.96E+05			
NI2O3							7.29E-03			
NEO2							1.96E-05			
PO2							3.06E+03			
FSO2							6.26E+02			
FLU2							4.92E-02			
SEO3							9.52E-02			
SiO2							3.26E-01			
SN2O							4.39E-07			
SO3							2.14E+03			
SOLIDS		3.79E+02				3.79E+02	3.79E+02			
SRD							2.53E-02			
TC2O7							2.59E+01			
TiO2							1.41E+01			
UCO							9.06E+02			
ZNO							7.04E+02			
ZRO2							1.22E+02			

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Table B-16 Phase 1 LAW Mass Balance for Batch PC2/16 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	3.98E+06				1.56E+06	2.42E+06	2.32E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	3.98E+06				1.56E+06	2.42E+06	7.73E+03	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
As+3									
As+5									
Ba+3									
Ba+2									
Be+2									
Bi+3									
C-14									
Ca+2									
CD+2									
Cl-									
Cl2	1.01E+04				1.01E+04				
ClO2	3.65E+04				3.65E+04				
ClO3-2									
CR(OH)4-									
CS+									
Cl+2									
EU-154									
F-									
F2	7.12E+01				7.12E+01				
FE+3	2.42E+06					2.42E+06			
H2O									
HE+2									
K+									
La+3									
Mg+2									
Mn+4									
MO+6									
Na+							4.44E+03	5.75E-10	
Ni+3									
NO2	4.92E+05				4.92E+05				
NO2-									
NO3-									
NE+4									
O2	1.02E+06				1.02E+06				1.00E+06
OH-									
EB+4							3.25E+03	4.25E-10	
FO4-3									
FU+4									
SE+6									
SI+4									
SM+4									
SO4-2									
SR+2									
TiO4-									
TI+4									
TCC									
UD2+2									
ZN+2									
ZR+4									

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Table B-16 Phase 1 LAW Mass Balance for Batch PC2/16 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		7.98E+05	2.73E+06	3.53E+06					
RADIONUCLIDES (Ci)									
Cesium		3.39E+03		3.39E+03					
Strontium		2.99E+03		2.99E+03					
Technetium		2.81E+02		2.81E+02					
TRU		5.42E+00		5.42E+00					
CHEMICALS (kg)									
Ag2O		4.58E-04		4.58E-04					
Al2O3		1.02E+05		1.02E+05					
Am2O3		7.40E-04		7.40E-04					
As2O3		3.77E-04		3.77E-04					
BaO3		4.01E-02		4.01E-02					
BaO		9.16E-04		9.16E-04					
BaD		1.52E-04		1.52E-04					
BaZrO3		2.31E-07		2.31E-07					
CaO		8.30E+01		8.30E+01					
CaD		3.47E-04		3.47E-04					
CaZrO3		5.24E+02		5.24E+02					
Ce2O		4.14E-02		4.14E-02					
CUO		1.73E-08		1.73E-08					
Eu2O3		2.44E-12		2.44E-12					
Fe2O3		1.73E+00		1.73E+00					
FORMER			2.73E+06	2.73E+06					
H2O		9.93E-07		9.93E-07					
HMbAT									
K2O		9.10E+04		9.10E+04					
La2O3		5.69E-03		5.69E-03					
MgO		1.55E+02		1.55E+02					
MnO2		7.43E+01		7.43E+01					
MOO3		1.55E+02		1.55E+02					
Na2O		5.96E+05		5.96E+05					
Ni2O3		7.29E-03		7.29E-03					
NiO2		1.96E-05		1.96E-05					
P2O5		3.06E+03		3.06E+03					
PbO2		6.26E+02		6.26E+02					
PLU2		4.92E-02		4.92E-02					
SEO3		9.52E-02		9.52E-02					
SiO2		3.26E-01		3.26E-01					
SnO2		4.39E-07		4.39E-07					
SO3		2.14E+03		2.14E+03					
SOLIDS		3.79E+02		3.79E+02					
SrO		2.53E-02		2.53E-02					
Ta2O7		2.59E+01		2.59E+01					
TiO2		1.41E+01		1.41E+01					
UD3		9.06E+02		9.06E+02					
ZrO		7.04E+02		7.04E+02					
ZrO2		1.22E+02		1.22E+02					

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Table B-17 Phase 1 LAW Mass Balance for Batch PC2/17 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.51E+06	3.49E+06	1.71E+04	4.16E+05	4.33E+05		3.49E+06	3.49E+06		
Density (g/L)	1.41E+03	1.41E+03	1.41E+03	1.00E+03	1.02E+03		1.41E+03	1.41E+03		
Total Mass Flow (kg)	4.93E+06	4.91E+06	2.41E+04	4.16E+05	4.40E+05		4.91E+06	4.91E+06		
RADIONUCLIDES (Ci)										
Cesium	1.34E+06	1.33E+06	6.53E+03		6.53E+03		1.33E+06	1.33E+06		
Strontium	2.22E+04	2.21E+04	1.09E+02		1.09E+02		2.21E+04	2.21E+04		
Technetium	3.06E+02	3.06E+02	1.50E+00		1.50E+00		3.06E+02	3.06E+02		
TU1	8.32E+00	8.28E+00	4.07E-02		4.07E-02		8.28E+00	8.28E+00		
CHEMICALS (kg)										
AGP	2.02E-05	2.01E-05	9.88E-08		9.88E-08		2.01E-05	2.01E-05		
AL(OH)4-	3.57E+05	3.55E+05	1.74E+03		1.74E+03		3.55E+05	3.55E+05		
AM+3	1.18E-03	1.18E-03	5.79E-06		5.79E-06		1.18E-03	1.18E-03		
ASH+5	1.17E-05	1.16E-05	5.70E-08		5.70E-08		1.16E-05	1.16E-05		
BH+1	5.85E-04	5.82E-04	2.82E-06		2.82E-06		5.82E-04	5.82E-04		
BH+2	3.89E-05	3.87E-05	1.90E-07		1.90E-07		3.87E-05	3.87E-05		
BE+2	2.60E-06	2.59E-06	1.27E-08		1.27E-08		2.59E-06	2.59E-06		
BI+3	9.85E-09	9.80E-09	4.81E-11		4.81E-11		9.80E-09	9.80E-09		
C-14	7.70E-04	7.66E-04	3.76E-06		3.76E-06		7.66E-04	7.66E-04		
CA+2	1.50E+02	1.50E+02	7.35E-01		7.35E-01		1.50E+02	1.50E+02		
CD+2	2.71E+01	2.70E+01	1.33E-01		1.33E-01		2.70E+01	2.70E+01		
CL-	1.69E+04	1.69E+04	8.28E+01		8.28E+01		1.69E+04	1.69E+04		
CL2										
CO2										
CO3-2	1.69E+04	1.69E+04	8.28E+01		8.28E+01		1.69E+04	1.69E+04		
CO3(OH)4-	3.97E+03	3.93E+03	1.65E+01		1.65E+01		3.93E+03	3.93E+03		
CS+	1.55E+01	1.54E+01	7.56E-02		7.56E-02		1.54E+01	1.54E+01		
CU+2	2.03E+01	2.02E+01	9.92E-02		9.92E-02		2.02E+01	2.02E+01		
F-	1.25E+03	1.25E+03	6.12E+00		6.12E+00		1.25E+03	1.25E+03		
F2										
FE+3	1.19E+02	1.19E+02	5.63E-01	4.16E+05	5.83E-01		1.19E+02	1.19E+02		
H2O	3.16E+06	3.15E+06	1.53E+04		4.31E+05		3.15E+06	3.15E+06		
HE+2	2.71E+01	2.70E+01	1.33E-01		1.33E-01		2.70E+01	2.70E+01		
HF	3.11E+04	3.10E+04	1.52E+02		1.52E+02		3.10E+04	3.10E+04		
LAH+3	2.30E-04	2.29E-04	1.12E-06		1.12E-06		2.29E-04	2.29E-04		
MG+2	5.55E+01	5.52E+01	2.71E-01		2.71E-01		5.52E+01	5.52E+01		
MNH+4	5.21E+01	5.18E+01	2.55E-01		2.55E-01		5.18E+01	5.18E+01		
MD+6	1.56E+02	1.56E+02	7.64E-01		7.64E-01		1.56E+02	1.56E+02		
NA+	6.00E+05	5.97E+05	2.93E+03		2.93E+03		5.97E+05	5.97E+05		
NH+3	4.06E+01	4.04E+01	1.99E-01		1.99E-01		4.04E+01	4.04E+01		
NO2										
NO2-	2.47E+05	2.46E+05	1.21E+03		1.21E+03		2.46E+05	2.46E+05		
NO3-	2.99E+05	2.98E+05	1.46E+03		1.46E+03		2.98E+05	2.98E+05		
NH+4	4.80E-02	4.78E-02	2.35E-04		2.35E-04		4.78E-02	4.78E-02		
O2										
OH-	1.76E+05	1.75E+05	8.61E+02		8.61E+02		1.75E+05	1.75E+05		
OH+4	1.61E+02	1.60E+02	7.85E-01		7.85E-01		1.60E+02	1.60E+02		
FO4-3	1.86E+03	1.85E+03	9.08E+00		9.08E+00		1.85E+03	1.85E+03		
EU+4	5.83E-02	5.80E-02	2.85E-04		2.85E-04		5.80E-02	5.80E-02		
SE+6	4.23E-03	4.20E-03	2.07E-05		2.07E-05		4.20E-03	4.20E-03		
SI+4	4.61E+02	4.58E+02	2.25E+00		2.25E+00		4.58E+02	4.58E+02		
SN+4	1.63E-08	1.63E-08	7.98E-11		7.98E-11		1.63E-08	1.63E-08		
SO4-2	2.86E+03	2.86E+03	1.41E+01		1.41E+01		2.86E+03	2.86E+03		
SR+2	1.60E-01	1.59E-01	7.81E-04		7.81E-04		1.59E-01	1.59E-01		
TU+4	2.98E+01	2.97E+01	1.44E-01		1.44E-01		2.97E+01	2.97E+01		
TI+4	6.03E-01	6.00E-01	2.95E-03		2.95E-03		6.00E-01	6.00E-01		
TIC	1.26E+04	1.27E+04	6.25E+01		6.25E+01		1.27E+04	1.27E+04		
UD2+2	6.29E+01	6.26E+01	3.07E-01		3.07E-01		6.26E+01	6.26E+01		
WH+6	3.53E+02	3.51E+02	1.72E+00		1.72E+00		3.51E+02	3.51E+02		
ZN+2	1.22E+02	1.21E+02	5.95E-01		5.95E-01		1.21E+02	1.21E+02		
Zn+4	6.44E+00	6.41E+00	3.15E-02		3.15E-02		6.41E+00	6.41E+00		

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Table B-17 Phase 1 LAW Mass Balance for Batch PC2/17 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.93E+04	4.93E+02	4.88E+04		4.88E+04		4.93E+02	4.93E+02		
RADIONUCLIDES (Ci)										
Cesium										
Strontium										
Technetium										
TBU										
CHEMICALS (kg)										
Ag2O										
Al2O3										
Am2O3										
As2O5										
B2O3										
BaO										
BzO										
Bi2O3										
CaO										
ClO										
Cr2O3										
Cs2O										
ClO										
Fe2O3										
FURMER										
H2O										
LiAlH4										
K2O										
La2O3										
Me3										
MnO2										
MnO3										
Na2O										
Ni2O3										
NeO2										
Fe2O5										
FeO2										
Flu2										
SeO3										
SiO2										
SnO2										
SO3										
SULFURS	4.93E+04	4.93E+02	4.88E+04		4.88E+04		4.93E+02	4.93E+02		
SO										
Ti2O7										
TiO2										
UO3										
W3										
ZnO										
ZrO2										

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Table B-17 Phase 1 LAW Mass Balance for Batch PC2/17 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.49E+06	3.14E+03		3.14E+03	3.49E+06	4.87E+06		1.00E+09	1.00E+09
Density (g/L)		1.41E+03	3.32E+03		3.32E+03	1.41E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.91E+06	1.05E+04		1.05E+04	4.91E+06	4.87E+06		1.00E+09	1.00E+09
RADIONUCLIDES (Ci)										
Cesium		4.57E+03	1.33E+06		1.33E+06	4.57E+03				
Strontium		2.21E+04			2.21E+04	2.21E+04				
Technetium		3.03E+02	3.08E+00		3.08E+00	3.03E+02				
TRU		8.22E+00			8.22E+00	8.22E+00				
CHEMICALS (kg)										
AG+		2.01E-05				2.01E-05				
AL(OH)4-		3.55E+05				3.55E+05				
AM+3		1.18E-03				1.18E-03				
AS+5		1.16E-05				1.16E-05				
BE+3		5.86E-04				5.86E-04				
BE+2		3.87E-05				3.87E-05				
BE+2		2.59E-06				2.59E-06				
BE+3		9.80E-09				9.80E-09				
C-14		7.66E-04				7.66E-04				
CA+2		1.50E+02				1.50E+02				
CD+2		2.70E+01				2.70E+01				
CL-		1.69E+04				1.69E+04				
CL2							1.69E+04			
CO2							5.90E+04			
CO3-2		1.69E+04				1.69E+04				
CR(OH)4-		3.35E+03				3.35E+03				
CS+		5.28E-02	1.53E+01		1.53E+01	5.28E-02				
CU+2		2.02E+01				2.02E+01				
F-		1.25E+03				1.25E+03				
F2							1.25E+03			
FE+3		1.19E+02				1.19E+02				
H2O		3.15E+06				3.15E+06	3.38E+06		1.00E+09	1.00E+09
HG+2		2.70E+01				2.70E+01				
K+		3.10E+04				3.10E+04				
LA+3		2.29E-04				2.29E-04				
ME+2		5.52E+01				5.52E+01				
MN+4		5.18E+01				5.18E+01				
ND+6		1.56E+02				1.56E+02				
NA+		5.97E+05	6.00E+03		6.00E+03	5.97E+05				
NH+3		4.04E+01				4.04E+01				
NO2							4.67E+05			
NO2-		2.46E+05				2.46E+05				
NO3-		2.98E+05				2.98E+05				
NE+4		4.78E-02				4.78E-02				
O2							9.46E+05			
OH-		1.75E+05	4.44E+03		4.44E+03	1.75E+05				
EB+4		1.60E+02				1.60E+02				
FO4-3		1.85E+03				1.85E+03				
FI+4		5.80E-02				5.80E-02				
SE+6		4.20E-03				4.20E-03				
SI+4		4.58E+02				4.58E+02				
SN+4		1.63E-08				1.63E-08				
SO4-2		2.86E+03				2.86E+03				
SR+2		1.59E-01				1.59E-01				
TICM+		2.94E+01	2.98E-01		2.98E-01	2.94E+01				
TI+4		6.00E-01				6.00E-01				
TIC2		1.27E+04				1.27E+04				
UO2+2		6.26E+01				6.26E+01				
WH6		3.51E+02				3.51E+02				
ZN+2		1.21E+02				1.21E+02				
ZR+4		6.41E+00				6.41E+00				

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Table B-17 Phase 1 LAW Mass Balance for Batch PC2/17 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.93E+02		6.00E+03	6.00E+03	4.93E+02	1.04E+06			
RADIONUCLIDES (Ci)										
Cesium							4.57E+03			
Strontium							2.21E+04			
Technetium							3.03E+02			
TU							8.23E+00			
CHEMICALS (kg)										
AG2O							2.16E-05			
AL2O3							1.91E+05			
AM2O3							1.30E-03			
AS2O3							1.78E-05			
B2O3							1.89E-03			
BAO							4.32E-05			
BAO							7.18E-06			
BI2O3							1.09E-08			
CaO							2.09E+02			
ClO							3.08E+01			
CR2O3							2.12E+03			
CS2O							5.59E-02			
CU							2.53E+01			
FE2O3							1.70E+02			
FORMER										
HEO							2.92E+01			
DMAT										
K2O				6.00E+03	6.00E+03					
LA2O3							3.73E+04			
MFO							2.68E-04			
MFO							9.15E+01			
MNO2							8.20E+01			
MCO3							2.34E+02			
Na2O							8.04E+05			
NI2O3							5.69E+01			
NEO2							5.43E-02			
PO5							1.38E+03			
PBO2							1.85E+02			
PUO2							6.53E-02			
SEO3							6.76E-03			
STO2							9.80E+02			
SN2							2.06E-08			
SO3							2.39E+03			
SOLIDS		4.93E+02				4.93E+02	4.93E+02			
SFO							1.87E-01			
TC2O7							2.79E+01			
TIO2							1.00E+00			
UO3							6.63E+01			
VO3							4.42E+02			
ZNO							1.51E+02			
ZRO2							8.65E+00			

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Table B-17 Phase 1 LAW Mass Balance for Batch PC2/17 (6 sheets)

SIREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.87E+06				1.49E+06	3.38E+06	3.13E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	4.87E+06				1.49E+06	3.38E+06	1.04E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Cl)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
As+3									
As+5									
B+3									
BE+2									
BE+2									
BI+3									
C-14									
Ca+2									
CD+2									
CL-									
CL2	1.69E+04				1.69E+04				
CL2	5.90E+04				5.90E+04				
CO-2									
CR(OH)4-									
CS+									
CU+2									
F-									
F2	1.25E+03				1.25E+03				
FE+3									
H2O	3.38E+06					3.38E+06			
H3+2									
K+									
LA+3									
MG+2									
MN+4									
MO+6									
NA+							6.00E+03	5.75E-10	
NI+3									
NO2	4.67E+05				4.67E+05				
NO2-									
NO3-									
NE+4									
O2	9.46E+05				9.46E+05				1.00E+06
OH-							4.44E+03	4.25E-10	
PH+4									
PO4-3									
PU+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TIO4-									
TI+4									
TIC									
UC2+2									
WH6									
ZN+2									
ZR+4									

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Table B-17 Phase 1 LAW Mass Balance for Batch PC2/17 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		1.04E+06	3.72E+06	4.76E+06					
RADIONUCLIDES (Ci)									
Cesium		4.57E+03		4.57E+03					
Strontium		2.21E+04		2.21E+04					
Technetium		3.03E+02		3.03E+02					
TRU		8.23E+00		8.23E+00					
CHEMICALS (kg)									
Ag2O		2.16E-05		2.16E-05					
Al2O3		1.91E+05		1.91E+05					
Am2O3		1.30E-03		1.30E-03					
As2O5		1.78E-05		1.78E-05					
B2O3		1.89E-03		1.89E-03					
B4O7		4.32E-05		4.32E-05					
B2O		7.18E-06		7.18E-06					
Bi2O3		1.09E-08		1.09E-08					
CaO		2.09E+02		2.09E+02					
Cl2O		3.08E+01		3.08E+01					
Cr2O3		2.12E+03		2.12E+03					
CS2O		5.59E-02		5.59E-02					
CU2O		2.53E+01		2.53E+01					
Fe2O3		1.70E+02		1.70E+02					
FORMER			3.72E+06						
HEO		2.92E+01		2.92E+01					
DMBT									
K2O		3.73E+04		3.73E+04					
La2O3		2.68E-04		2.68E-04					
MgO		9.15E+01		9.15E+01					
MnO2		8.20E+01		8.20E+01					
MCO3		2.34E+02		2.34E+02					
Na2O		8.04E+05		8.04E+05					
Ni2O3		5.69E+01		5.69E+01					
NEO2		5.43E-02		5.43E-02					
P2O5		1.38E+03		1.38E+03					
PbO2		1.83E+02		1.83E+02					
PtO2		6.58E-02		6.58E-02					
SeO3		6.76E-03		6.76E-03					
SiO2		9.80E+02		9.80E+02					
SnO2		2.06E-08		2.06E-08					
SO3		2.39E+03		2.39E+03					
SOLIDS		4.93E+02		4.93E+02					
SrO		1.87E-01		1.87E-01					
TCCO7		2.79E+01		2.79E+01					
TiO2		1.00E+00		1.00E+00					
UO3		6.63E+01		6.63E+01					
VO3		4.42E+02		4.42E+02					
ZnO		1.51E+02		1.51E+02					
ZrO2		8.65E+00		8.65E+00					

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Table B-18 Phase 1 LAW Mass Balance for Batch PC2/18 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	1.06E+06	1.05E+06	6.85E+03	1.13E+05	1.20E+05		1.05E+06	1.05E+06		
Density (g/L)	1.25E+03	1.25E+03	1.25E+03	1.00E+03	1.02E+03		1.25E+03	1.25E+03		
Total Mass Flow (kg)	1.37E+06	1.36E+06	8.83E+03	1.13E+05	1.22E+05		1.36E+06	1.36E+06		
RADIONUCLIDES (Ci)										
Cesium	1.77E+06	1.75E+06	1.14E+04		1.14E+04		1.75E+06	1.75E+06		
Strontium	4.47E+03	4.44E+03	2.89E+01		2.89E+01		4.44E+03	4.44E+03		
Technetium	3.55E+02	3.52E+02	2.30E+00		2.30E+00		3.52E+02	3.52E+02		
TRU	3.48E+01	3.46E+01	2.25E-01		2.25E-01		3.46E+01	3.46E+01		
CHEMICALS (kg)										
AG+	6.14E-07	6.10E-07	3.98E-09		3.98E-09		6.10E-07	6.10E-07		
AL(OH)4-	4.01E+04	3.98E+04	2.60E+02		2.60E+02		3.98E+04	3.98E+04		
AM+3	5.56E-03	5.52E-03	3.60E-05		3.60E-05		5.52E-03	5.52E-03		
AS+5	3.54E-07	3.52E-07	2.29E-09		2.29E-09		3.52E-07	3.52E-07		
B+3	1.79E-05	1.78E-05	1.14E-07		1.16E-07		1.78E-05	1.78E-05		
BA+2	4.68E-02	4.65E-02	3.03E-04		3.03E-04		4.65E-02	4.65E-02		
BE+2	7.91E-08	7.85E-08	5.12E-10		5.12E-10		7.85E-08	7.85E-08		
BI+3	2.99E-10	2.97E-10	1.94E-12		1.94E-12		2.97E-10	2.97E-10		
C-14	4.24E-04	4.22E-04	2.75E-06		2.75E-06		4.22E-04	4.22E-04		
CA+2	8.81E+00	8.76E+00	5.70E-02		5.70E-02		8.76E+00	8.76E+00		
CD+2	1.30E+00	1.29E+00	8.39E-03		8.39E-03		1.29E+00	1.29E+00		
CL-	9.25E+02	9.19E+02	5.98E+00		5.98E+00		9.19E+02	9.19E+02		
CL2										
CO3-2										
CR(OH)4-	3.76E+04	3.73E+04	2.43E+02		2.43E+02		3.73E+04	3.73E+04		
CS+	2.46E+03	2.45E+03	1.59E+01		1.59E+01		2.45E+03	2.45E+03		
CS+	2.04E+01	2.03E+01	1.32E-01		1.32E-01		2.03E+01	2.03E+01		
CU+2	9.68E-01	9.61E-01	6.26E-03		6.26E-03		9.61E-01	9.61E-01		
EU-154	1.02E-02	1.01E-02	6.60E-05		6.60E-05		1.01E-02	1.01E-02		
F-	1.74E+03	1.73E+03	1.12E+01		1.12E+01		1.73E+03	1.73E+03		
F2										
FE+3	5.78E+00	5.74E+00	3.74E-02		3.74E-02		5.74E+00	5.74E+00		
HC0	9.68E+05	9.61E+05	6.26E+03	1.13E+05	1.19E+05		9.61E+05	9.61E+05		
HO+	1.30E+00	1.29E+00	8.39E-03		8.39E-03		1.29E+00	1.29E+00		
K+	4.22E+03	4.21E+03	2.74E+01		2.74E+01		4.21E+03	4.21E+03		
LA+3	4.99E-01	4.96E-01	3.23E-03		3.23E-03		4.96E-01	4.96E-01		
MD+2	2.68E+00	2.66E+00	1.73E-02		1.73E-02		2.66E+00	2.66E+00		
MN+4	2.45E+00	2.44E+00	1.59E-02		1.59E-02		2.44E+00	2.44E+00		
MO+6	7.38E+00	7.33E+00	4.78E-02		4.78E-02		7.33E+00	7.33E+00		
NA+	1.25E+05	1.25E+05	8.11E+02		8.11E+02		1.25E+05	1.25E+05		
NI+3	2.45E+00	2.44E+00	1.59E-02		1.59E-02		2.44E+00	2.44E+00		
NO2										
NO2-	6.71E+04	6.67E+04	4.33E+02		4.33E+02		6.67E+04	6.67E+04		
NO3-	7.40E+04	7.36E+04	4.79E+02		4.79E+02		7.36E+04	7.36E+04		
NE+4	1.05E-01	1.05E-01	6.62E-04		6.62E-04		1.05E-01	1.05E-01		
O2										
OH-	1.74E+04	1.73E+04	1.12E+02		1.12E+02		1.73E+04	1.73E+04		
PO4-3	7.22E+00	7.18E+00	4.68E-02		4.68E-02		7.18E+00	7.18E+00		
PO4-3	1.01E+03	1.00E+03	6.54E+00		6.54E+00		1.00E+03	1.00E+03		
PU+4	2.16E-01	2.15E-01	1.40E-03		1.40E-03		2.15E-01	2.15E-01		
SE+6	1.53E-04	1.52E-04	9.90E-07		9.90E-07		1.52E-04	1.52E-04		
SI+4	3.28E+02	3.25E+02	2.12E+00		2.12E+00		3.25E+02	3.25E+02		
SN+4	4.98E-10	4.94E-10	3.22E-12		3.22E-12		4.94E-10	4.94E-10		
SO4-2	2.08E+04	2.07E+04	1.35E+02		1.35E+02		2.07E+04	2.07E+04		
SO4-2	3.21E-02	3.19E-02	2.08E-04		2.08E-04		3.19E-02	3.19E-02		
TCD+4	3.44E+01	3.42E+01	2.23E-01		2.23E-01		3.42E+01	3.42E+01		
TI+4	2.19E-02	2.17E-02	1.42E-04		1.42E-04		2.17E-02	2.17E-02		
TCC	2.26E+03	2.25E+03	1.47E+01		1.47E+01		2.25E+03	2.25E+03		
UD2+2	1.90E+03	1.89E+03	1.23E+01		1.23E+01		1.89E+03	1.89E+03		
WH+6	1.69E+01	1.67E+01	1.09E-01		1.09E-01		1.67E+01	1.67E+01		
ZN+2	5.43E+00	5.39E+00	3.51E-02		3.51E-02		5.39E+00	5.39E+00		
ZR+4	2.33E-01	2.32E-01	1.51E-03		1.51E-03		2.32E-01	2.32E-01		

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Table B-18 Phase I LAW Mass Balance for Batch PC2/18 (6 sheets)

STREAM NAME SOLID COMPONENTS	1	2	3	4	5	6	7	8	9	10
Total Mass Flow (kg)	1.37E+04	1.37E+02	1.35E+04		1.35E+04		1.37E+02	1.37E+02		
RADIONUCLIDES (Cl)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
AG2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
BAO										
BeO										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
EL2O3										
FE2O3										
FORMER										
HO										
DMAT										
K2O										
LA2O3										
MO										
MNO2										
MCO3										
NA2O										
NIL2O3										
NFO2										
P2O5										
PRG2										
RU2										
SE03										
SiO2										
SN2										
SO3										
SOLIDS	1.37E+04	1.37E+02	1.35E+04		1.35E+04		1.37E+02	1.37E+02		
SRD										
TC2O7										
TiO2										
UO3										
W03										
ZNO										
ZRO2										

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Table B-18 Phase 1 LAW Mass Balance for Batch PC2/18 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		1.05E+06	6.74E+02		6.74E+02	1.05E+06	2.14E+06	6.64E+02	1.25E+03	1.92E+03
Density (g/L)		1.29E+03	3.27E+03		3.27E+03	1.29E+03	1.00E+03	3.30E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)		1.36E+06	2.20E+03		2.20E+03	1.36E+06	2.14E+06	2.19E+03	1.25E+03	3.44E+03
RADIONUCLIDES (Ci)										
Cesium		2.39E+03	1.75E+06		1.75E+06	2.39E+03				
Strontium		4.44E+03				4.44E+03				
Technetium		3.49E+02	3.53E+00		3.55E+00	2.39E+02		1.10E+02		1.10E+02
TU		3.46E+01				3.46E+01				
CHEMICALS (kg)										
AG+		6.10E-07				6.10E-07				
AL(OH)4-		3.98E+04				3.98E+04				
AM+3		5.52E-03				5.52E-03				
AS+5		3.52E-07				3.52E-07				
BI+3		1.78E-05				1.78E-05				
BI+2		4.65E-02				4.65E-02				
BE+2		7.85E-08				7.85E-08				
BI+3		2.97E-10				2.97E-10				
C-14		4.22E-04				4.22E-04				
CA+2		8.76E+00				8.76E+00				
CD+2		1.29E+00				1.29E+00				
CL-		9.19E+02				9.19E+02				
CL2								9.19E+02		
CO2								3.56E+04		
CO3-2		3.73E+04				3.73E+04				
CR(OH)4-		2.43E+03				2.43E+03				
CS+		2.76E-02	2.02E+01		2.02E+01	2.76E-02				
CH2		9.61E-01				9.61E-01				
EU-154		1.01E-02				1.01E-02				
F-		1.73E+03				1.73E+03				
F2								1.73E+03		
FE+3		5.74E+00				5.74E+00				
H2O		9.61E+05				9.61E+05		9.66E+05	1.25E+03	1.25E+03
HCl+2		1.29E+00				1.29E+00				
K+		4.21E+03				4.21E+03				
LA+3		4.96E-01				4.96E-01				
MF+2		2.66E+00				2.66E+00				
NH4+		2.44E+00				2.44E+00				
ND+6		7.33E+00				7.33E+00				
NA+		1.25E+05	1.25E+03		1.25E+03	1.25E+05		1.25E+03		1.25E+03
NI+3		2.44E+00				2.44E+00				
NO2								1.21E+05		
NO2-		6.67E+04				6.67E+04				
NO3-		7.36E+04				7.36E+04				
NH4+		1.05E-01				1.05E-01				
O2								9.94E+05		
OH-		1.73E+04	9.27E+02		9.27E+02	1.73E+04		9.27E+02		9.27E+02
BI+4		7.18E+00				7.18E+00				
RO4-3		1.00E+03				1.00E+03				
FI+4		2.15E-01				2.15E-01				
SE+6		1.52E-04				1.52E-04				
SI+4		3.25E+02				3.25E+02				
SN+4		4.94E-10				4.94E-10				
SO4-2		2.07E+04				2.07E+04				
SR+2		3.19E-02				3.19E-02				
TCl4		3.34E+01	3.44E-01		3.44E-01	2.31E+01		1.07E+01		1.07E+01
TI+4		2.17E-02				2.17E-02				
TCl3		2.25E+03				2.25E+03				
UO2+2		1.89E+03				1.89E+03				
W+6		1.67E+01				1.67E+01				
ZN+2		5.39E+00				5.39E+00				
ZR+4		2.32E-01				2.32E-01				

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Table B-18 Phase 1 LAW Mass Balance for Batch PC2/18 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		1.37E+02		1.25E+03	1.25E+03	1.37E+02	2.17E+05			
RADIONUCLIDES (Ci)										
Cesium							2.39E+03			
Strontium							4.44E+03			
Technetium							2.39E+02			
TU							3.44E+01			
CHEMICALS (kg)										
AC2O							6.56E-07			
AL2O3							2.14E+04			
AM2O3							6.07E-03			
AS2O3							5.40E-07			
B2O3							5.72E-05			
BAO							5.20E-02			
BB2O3							2.18E-07			
Bi2O3							3.31E-10			
CaO							1.23E+01			
Cl2O							1.47E+00			
CR2O3							1.53E+03			
CS2O							2.92E-02			
CU2O							1.20E+00			
EU2O3							1.17E-02			
FE2O3							8.21E+00			
FURMER										
H2O				1.25E+03	1.25E+03		1.39E+00			
DMAT										
K2O							5.07E+03			
LA2O3							5.82E-01			
Na2O							4.41E+00			
NH2O							3.86E+00			
MO3							1.10E+01			
NA2O							1.68E+05			
NI2O3							3.43E+00			
NH2O							1.19E-01			
Fe2O5							7.51E+02			
FeO2							8.29E+00			
HUO2							2.44E-01			
SD2O							2.44E-04			
SiO2							6.96E+02			
SN2O							6.28E-10			
SO3							1.72E+04			
SULFUS		1.37E+02				1.37E+02	1.37E+02			
SO2							3.76E-02			
TC2O7							2.20E+01			
TiO2							3.62E-02			
UO3							2.00E+03			
WO3							2.11E+01			
ZNO							6.71E+00			
ZrO2							3.13E-01			

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Table B-18 Phase 1 LAW Mass Balance for Batch PC2/18 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	2.14E+06				1.15E+06	9.86E+05	6.54E+02	6.54E+02	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	2.14E+06				1.15E+06	9.86E+05	2.18E+03	2.18E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AN+3									
AS+5									
BH+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	9.19E+02				9.19E+02				
CO2	3.56E+04				3.56E+04				
CO3-2									
CR(OH)4-									
CS+									
CH2									
EU-154									
F-									
F2	1.73E+03				1.73E+03				
FE+3									
H2O	9.66E+05					9.86E+05			
H3+2									
K+									
LA+3									
MP+2									
MM+4									
ND+6									
NA+							1.25E+03	1.25E+03	
NI+3									
NO2	1.21E+05				1.21E+05				
NO2-									
NO3-									
NE+4									
O2	9.94E+05				9.94E+05				1.00E+06
OH-							9.27E+02	9.27E+02	
FB+4									
FW-3									
FU+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TOD-									
TI+4									
TC									
UD2+2									
WH6									
ZH+2									
ZR+4									

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Table B-18 Phase 1 LAW Mass Balance for Batch PC2/18 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		2.17E+05	2.27E+06	2.49E+06					
RADIONUCLIDES (Ci)									
Cesium		2.39E+03		2.39E+03					
Strontium		4.44E+03		4.44E+03					
Technetium		2.39E+02		2.39E+02					
TU		3.44E+01		3.44E+01					
CHEMICALS (kg)									
ACG0		6.56E-07		6.56E-07					
AL2O3		2.14E+04		2.14E+04					
AM2O3		6.07E-03		6.07E-03					
AS2O3		5.40E-07		5.40E-07					
B2O3		5.72E-05		5.72E-05					
B4O		5.20E-02		5.20E-02					
BBO		2.18E-07		2.18E-07					
BL2O3		3.31E-10		3.31E-10					
CaO		1.23E+01		1.23E+01					
ClO		1.47E+00		1.47E+00					
CR2O3		1.55E+03		1.55E+03					
CS2O		2.92E-02		2.92E-02					
CU		1.20E+00		1.20E+00					
EU2O3		1.17E-02		1.17E-02					
FE2O3		8.21E+00		8.21E+00					
FORMER			2.27E+06	2.27E+06					
H2O		1.39E+00		1.39E+00					
DMAT									
K2O		5.07E+03		5.07E+03					
LA2O3		5.82E-01		5.82E-01					
M2O		4.41E+00		4.41E+00					
M2O2		3.86E+00		3.86E+00					
M2O3		1.10E+01		1.10E+01					
NA2O		1.68E+05		1.68E+05					
NIL2O3		3.43E+00		3.43E+00					
NEO2		1.19E-01		1.19E-01					
PO5		7.51E+02		7.51E+02					
PBO2		8.29E+00		8.29E+00					
PUO2		2.44E-01		2.44E-01					
SEO3		2.44E-04		2.44E-04					
SiO2		6.96E+02		6.96E+02					
SnO2		6.28E-10		6.28E-10					
SO3		1.72E+04		1.72E+04					
SOLIDS		1.37E+02		1.37E+02					
SHO		3.76E-02		3.76E-02					
TC2O7		2.20E+01		2.20E+01					
TiO2		3.62E-02		3.62E-02					
UO3		2.00E+03		2.00E+03					
WO3		2.11E+01		2.11E+01					
ZNO		6.71E+00		6.71E+00					
ZrO2		3.13E-01		3.13E-01					

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Table B-19 Phase 1 LAW Mass Balance for Batch PC2/19 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	7.51E+05	7.47E+05	3.66E+03	8.30E+04	8.66E+04		7.47E+05	7.47E+05	3.66E+01	8.36E+02
Density (g/L)	1.31E+03	1.31E+03	1.31E+03	1.00E+03	1.01E+03		1.31E+03	1.31E+03	1.31E+03	1.00E+03
Total Mass Flow (kg)	9.86E+05	9.81E+05	4.80E+03	8.30E+04	8.78E+04		9.81E+05	9.81E+05	4.84E+01	8.36E+02
RADIONUCLIDES (Ci)										
Cesium	3.14E+05	3.12E+05	1.53E+03		1.53E+03		3.12E+05	3.12E+05	1.54E+01	
Strontium	4.48E+04	4.46E+04	2.18E+02		2.18E+02		5.72E+03	5.72E+03	2.82E-01	
Technetium	1.87E+02	1.86E+02	9.13E-01		9.13E-01		1.86E+02	1.86E+02	9.19E-03	
IU1	3.20E+02	3.19E+02	1.56E+00		1.56E+00		8.11E+01	8.11E+01	4.00E-03	
CHEMICALS (kg)										
AGP	5.23E-08	5.20E-08	2.55E-10		2.55E-10		5.20E-08	5.20E-08	2.57E-12	
AL(OH)4-	6.09E+03	6.06E+03	2.97E+01		2.97E+01		6.06E+03	6.06E+03	2.99E-01	
AM3	8.81E-02	8.77E-02	4.29E-04		4.29E-04		2.23E-02	2.23E-02	1.10E-06	
ASH5	3.02E-08	3.00E-08	1.47E-10		1.47E-10		3.00E-08	3.00E-08	1.48E-12	
BP3	1.52E-06	1.51E-06	7.41E-09		7.41E-09		1.51E-06	1.51E-06	7.46E-11	
BM2	5.03E-03	5.02E-03	2.45E-05		2.45E-05		5.00E-03	5.00E-03	2.47E-07	
BM2	2.93E-09	2.90E-09	3.28E-11		3.28E-11		6.70E-09	6.70E-09	3.30E-12	
BI+3	2.54E-11	2.53E-11	1.24E-13		1.24E-13		2.53E-11	2.53E-11	1.25E-15	
C-14	4.50E-05	4.48E-05	2.19E-07		2.19E-07		4.48E-05	4.48E-05	2.21E-09	
CA2	2.65E+02	2.64E+02	1.29E+00		1.29E+00		2.64E+02	2.64E+02	1.30E-02	
CD+2	1.21E-01	1.20E-01	5.89E-04		5.89E-04		1.20E-01	1.20E-01	5.93E-06	
CL-	1.58E+03	1.57E+03	7.70E+00		7.70E+00		1.57E+03	1.57E+03	7.76E-02	
CL2										
CO2										
CO3-2	4.01E+04	3.99E+04	1.93E+02		1.93E+02		3.99E+04	3.99E+04	1.97E+00	
CR(OH)4-	4.51E+02	4.49E+02	2.20E+00		2.20E+00		4.49E+02	4.49E+02	2.21E-02	
CSH	3.62E+00	3.60E+00	1.74E-02		1.74E-02		3.60E+00	3.60E+00	1.76E-04	
ClH2	9.07E-02	9.03E-02	4.42E-04		4.42E-04		9.03E-02	9.03E-02	4.43E-06	
EU-154	1.10E-03	1.09E-03	5.35E-06		5.35E-06		1.09E-03	1.09E-03	5.38E-08	
F-	1.86E+02	1.85E+02	9.05E-01		9.05E-01		1.85E+02	1.85E+02	9.11E-03	
F2										
FE+3	7.21E+02	7.18E+02	3.52E+00		3.52E+00		7.18E+02	7.18E+02	3.54E-02	
HO2	6.21E+05	6.18E+05	3.03E+03	8.30E+04	8.60E+04		6.18E+05	6.18E+05	3.05E+01	8.36E+02
HG+2	1.21E-01	1.20E-01	5.89E-04		5.89E-04		1.20E-01	1.20E-01	5.93E-06	
K+	1.45E+03	1.44E+03	7.07E+00		7.07E+00		1.44E+03	1.44E+03	7.12E-02	
Li+3	5.37E-02	5.34E-02	2.61E-04		2.61E-04		5.34E-02	5.34E-02	2.63E-06	
MH+2	2.53E-01	2.49E-01	1.22E-03		1.22E-03		2.49E-01	2.49E-01	1.23E-05	
NH+4	2.40E+02	2.40E+02	1.17E+00		1.17E+00		2.40E+02	2.40E+02	1.18E-02	
ND+6	6.87E-01	6.84E-01	3.35E-03		3.35E-03		6.84E-01	6.84E-01	3.37E-05	
Na+	1.20E+05	1.20E+05	5.85E+02		5.85E+02		1.20E+05	1.20E+05	5.89E+00	
NI+3	2.17E+02	2.16E+02	1.06E+00		1.06E+00		2.16E+02	2.16E+02	1.06E-02	
NO2										
NO2-	3.08E+04	3.06E+04	1.50E+02		1.50E+02		3.06E+04	3.06E+04	1.51E+00	
NO3-	1.22E+05	1.21E+05	5.94E+02		5.94E+02		1.21E+05	1.21E+05	5.98E+00	
NE+4	1.13E-02	1.13E-02	5.51E-05		5.51E-05		1.13E-02	1.13E-02	5.55E-07	
O2										
OH-	1.04E+04	1.03E+04	5.03E+01		5.03E+01		1.03E+04	1.03E+04	5.09E-01	
FB+4	1.59E+02	1.58E+02	7.75E-01		7.75E-01		1.58E+02	1.58E+02	7.80E-03	
FC+3	3.62E+02	3.60E+02	1.76E+00		1.76E+00		3.60E+02	3.60E+02	1.78E-02	
FU+4	2.48E-01	2.46E-01	1.21E-03		1.21E-03		6.29E-02	6.29E-02	3.10E-06	
SE+6	1.36E-05	1.35E-05	6.61E-08		6.61E-08		1.35E-05	1.35E-05	6.66E-10	
SI+4	3.49E+01	3.47E+01	1.70E-01		1.70E-01		3.47E+01	3.47E+01	1.71E-03	
SN+4	4.23E-11	4.21E-11	2.06E-13		2.06E-13		4.21E-11	4.21E-11	2.08E-15	
SO4-2	8.81E+03	8.77E+03	4.29E+01		4.29E+01		8.77E+03	8.77E+03	4.32E-01	
SR+2	3.22E-01	3.21E-01	1.57E-03		1.57E-03		4.11E-02	4.11E-02	2.03E-06	
TCO4-	1.81E+01	1.81E+01	8.84E-02		8.84E-02		1.81E+01	1.81E+01	8.90E-04	
TI+4	1.94E-03	1.93E-03	9.43E-06		9.43E-06		1.93E-03	1.93E-03	9.50E-08	
TCO	2.06E+04	2.07E+04	1.01E+02		1.01E+02		2.07E+04	2.07E+04	1.02E+00	
UCO+2	4.33E+02	4.31E+02	2.11E+00		2.11E+00		4.31E+02	4.31E+02	2.13E-02	
WH6	1.57E+00	1.57E+00	7.66E-03		7.66E-03		1.57E+00	1.57E+00	7.72E-05	
ZH+2	5.01E-01	4.99E-01	2.44E-03		2.44E-03		4.99E-01	4.99E-01	2.46E-05	
ZR+4	2.07E-02	2.06E-02	1.01E-04		1.01E-04		2.06E-02	2.06E-02	1.02E-06	

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Table B-19 Phase 1 LAW Mass Balance for Batch PC2/19 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	9.85E+03	9.85E+01	9.75E+03		9.75E+03		9.92E+01	9.92E-01	9.82E+01	
RADIONUCLIDES (Ci)										
Cesium										
Strontium							3.89E+04	3.89E+02	3.85E+04	
Technetium										
TRU							2.38E+02	2.38E+00	2.35E+02	
CHEMICALS (kg)										
AC2O										
AL2O3										
AMH3							6.54E-02	6.54E-04	6.47E-02	
AM2O3										
AS2O5										
B2O3										
B4O										
B2O										
Bi2O3										
CaO										
ClO										
CR2O3										
CS2O										
ClO										
EU2O3										
FE2O3										
FORMER										
H2O										
DMPT										
K2O										
LA2O3										
MO										
MN2										
MO3										
NA2O										
NI2O3										
NEO2										
OH-							1.72E-01	1.72E-03	1.70E-01	
P2O5										
PO2										
P3H4							1.84E-01	1.84E-03	1.82E-01	
PUD2										
SEO3										
SiO2										
SiO2										
SO3										
SOLIDS	9.85E+03	9.85E+01	9.75E+03		9.75E+03		9.85E+01	9.85E-01	9.75E+01	
SRH2							2.80E-01	2.80E-03	2.77E-01	
SRH										
TC2O7										
TiO2										
UO3										
UO3										
UO3										
ZNO										
ZRO2										

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Table B-19 Phase 1 LAW Mass Balance for Batch PC2/19 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	8.72E+02	7.47E+05	6.30E+02		6.30E+02	7.47E+05	1.81E+06	6.36E+02	1.20E+03	1.84E+03
Density (g/L)	1.01E+03	1.31E+03	3.32E+03		3.32E+03	1.31E+03	1.00E+03	3.30E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)	8.84E+02	9.81E+05	2.09E+03		2.09E+03	9.81E+05	1.81E+06	2.10E+03	1.20E+03	3.30E+03
RADIONUCLIDES (Ci)										
Cesium	1.54E+01	9.16E+02	3.11E+05		3.11E+05	9.16E+02				
Strontium	2.82E-01	5.72E+03				5.72E+03				
Technetium	9.19E-03	1.85E+02	1.87E+00		1.87E+00	9.16E+01		9.29E+01		9.29E+01
TU	4.00E-03	8.11E+01				8.11E+01				
CHEMICALS (kg)										
Ag+	2.57E-12	5.20E-08				5.20E-08				
AL(OH) ₄ ⁻	2.99E-01	6.06E+03				6.06E+03				
As ³⁺	1.10E-06	2.23E-02				2.23E-02				
As ⁵⁺	1.48E-12	3.00E-08				3.00E-08				
B ³⁺	7.46E-11	1.51E-06				1.51E-06				
Be ²⁺	2.27E-07	5.00E-03				5.00E-03				
Be ²⁺	3.30E-13	6.70E-09				6.70E-09				
Bi ³⁺	1.29E-15	2.53E-11				2.53E-11				
C-14	2.21E-09	4.48E-05				4.48E-05				
Ca ²⁺	1.30E-02	2.64E+02				2.64E+02				
CD ²⁺	5.93E-06	1.20E-01				1.20E-01				
Cl ⁻	7.76E-02	1.57E+03				1.57E+03				
Cl ₂									1.57E+03	
CO ₂									1.05E+05	
CO ₃ ²⁻	1.97E+00	3.99E+04				3.99E+04				
CR(OH) ₄ ⁻	2.21E-02	4.49E+02				4.49E+02				
CS ⁺	1.78E-04	1.06E-02	3.59E+00		3.59E+00	1.06E-02				
Cl ₂	4.45E-06	9.03E-02				9.03E-02				
EU-154	5.38E-08	1.09E-03				1.09E-03				
F ⁻	9.11E-03	1.85E+02				1.85E+02				
F ₂								1.85E+02		
FE ³⁺	3.54E-02	7.18E+02				7.18E+02				
H ₂ O	8.66E+02	6.18E+05				6.18E+05	6.26E+05		1.20E+03	1.20E+03
Hg ²⁺	5.93E-06	1.20E-01				1.20E-01				
K ⁺	7.12E-02	1.44E+03				1.44E+03				
LA ³⁺	2.63E-06	5.34E-02				5.34E-02				
Li ²⁺	1.23E-05	2.49E-01				2.49E-01				
Mn ⁴⁺	1.18E-02	2.40E+02				2.40E+02				
MO ⁶⁺	3.37E-05	6.84E-01				6.84E-01				
Na ⁺	5.89E+00	1.20E+05	1.20E+03		1.20E+03	1.20E+05		1.20E+03		1.20E+03
Ni ³⁺	1.06E-02	2.16E+02				2.16E+02				
NO ₂								1.21E+05		
NO ₂ ⁻	1.51E+00	3.06E+04				3.06E+04				
NO ₃ ⁻	5.98E+00	1.21E+05				1.21E+05				
NE ⁴⁺	5.59E-07	1.13E-02				1.13E-02				
O ₂								9.51E+05		
Cl	5.09E-01	1.03E+04	8.89E+02		8.89E+02	1.03E+04		8.89E+02		8.89E+02
EB ⁴⁺	7.80E-03	1.58E+02				1.58E+02				
FO ₄ ³⁻	1.78E-02	3.60E+02				3.60E+02				
Fl ⁴⁺	3.10E-06	6.29E-02				6.29E-02				
SE ⁶⁺	6.66E-10	1.35E-05				1.35E-05				
SI ⁴⁺	1.71E-03	3.47E+01				3.47E+01				
SN ⁴	2.08E-15	4.21E-11				4.21E-11				
SO ₄ ²⁻	4.32E-01	8.77E+03				8.77E+03				
SR ²⁺	2.03E-06	4.11E-02				4.11E-02				
Ti ₄ ⁺	6.90E-04	1.79E+01	1.81E-01		1.81E-01	8.07E+00		9.00E+00		9.00E+00
Ti ⁴⁺	9.50E-08	1.93E-03				1.93E-03				
TiC	1.02E+00	2.07E+04				2.07E+04				
UC ₂ ²⁺	2.13E-02	4.31E+02				4.31E+02				
WH ₆	7.72E-05	1.57E+00				1.57E+00				
ZN ²⁺	2.46E-05	4.99E-01				4.99E-01				
Zr ⁴⁺	1.02E-06	2.06E-02				2.06E-02				

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Table B-19 Phase 1 LAW Mass Balance for Batch PC2/19 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	9.82E+01	9.92E-01		1.20E+03	1.20E+03	9.92E-01	1.77E+05			
RADIONUCLIDES (Cl)										
Cesium							9.16E+02			
Strontium	3.83E+04	3.89E+02				3.89E+02	6.11E+03			
Technetium							9.16E+01			
TU1	2.35E+02	2.38E+00				2.38E+00	8.12E+01			
CHEMICALS (kg)										
AC20							5.59E-08			
AL2O3							3.25E+03			
AN#3	6.47E-02	6.54E-04				6.54E-04				
AN2O3							2.53E-02			
AS2O5							4.60E-08			
B2O3							4.87E-06			
B4O							5.59E-03			
B2O							1.86E-08			
BL2O3							2.82E-11			
CaO							3.69E+02			
ClO							1.38E-01			
CR2O3							2.84E+02			
CS2O							1.12E-02			
CUO							1.13E-01			
EU2O3							1.26E-03			
FE2O3							1.03E+03			
FURNER										
H2O							1.30E-01			
DMAC				1.20E+03	1.20E+03					
K2O							1.74E+03			
LA2O3							6.26E-02			
MO							4.14E-01			
MNO2							3.80E+02			
MCO3							1.03E+00			
NA2O							1.61E+05			
NI2O3							3.04E+02			
NEO2							1.28E-02			
CH-	1.70E-01	1.72E-03				1.72E-03				
FD25							2.69E+02			
FE2O2							1.83E+02			
FL#4	1.82E-01	1.84E-03				1.84E-03				
FUC2							7.34E-02			
SBO3							2.17E-05			
SIO2							7.43E+01			
SNO2							5.35E-11			
SO3							7.31E+03			
SULFIDS	9.75E+01	9.85E-01				9.85E-01	9.85E-01			
SR#2	2.77E-01	2.80E-03				2.80E-03				
SFO							5.17E-02			
TC207							8.44E+00			
TI02							3.21E-03			
UD3							4.57E+02			
UD3							1.97E+00			
ZNO							6.21E-01			
ZNO2							2.79E-02			

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Table B-19 Phase 1 LAW Mass Balance for Batch PC2/19 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	1.81E+06				1.18E+06	6.26E+05	6.27E+02	6.27E+02	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	1.81E+06				1.18E+06	6.26E+05	2.09E+03	2.09E+03	1.00E+06

RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									

CHEMICALS (kg)									
AG+									
AL(OH) ₃									
AN#3									
AS#5									
B#3									
B#4#2									
BE#2									
BI#3									
C-14									
CA#2									
CD#2									
CL-									
CL2	1.57E+03				1.57E+03				
CO2	1.05E+05				1.05E+05				
CO3-2									
CR(OH) ₃									
CS#									
CL#2									
EU-154									
F-									
F2	1.85E+02				1.85E+02				
FE#3									
H2O	6.26E+05					6.26E+05			
H3#2									
K+									
LA#3									
NA#2									
NA#4									
MD#6									
NA+							1.20E+03	1.20E+03	
NI#3									
NO2	1.21E+05				1.21E+05				
NO2-									
NO3-									
NE#4									
O2	9.51E+05				9.51E+05				1.00E+06
OH-							8.89E+02	8.89E+02	
IE#4									
FO#-3									
FU#4									
SE#6									
SI#4									
SN#4									
SO#-2									
SR#2									
TOD#									
TI#4									
TCC									
UC2#2									
WH#6									
ZH#2									
ZH#4									

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Table B-19 Phase 1 LAW Mass Balance for Batch PC2/19 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		1.77E+05	7.78E+05	9.54E+05					
RADIONUCLIDES (Ci)									
Cesium		9.16E+02		9.16E+02					
Strontium		6.11E+03		6.11E+03					
Technetium		9.16E+01		9.16E+01					
TRU		8.12E+01		8.12E+01					
CHEMICALS (kg)									
AG2O		5.59E-08		5.59E-08					
AL2O3		3.25E+03		3.25E+03					
AM+3									
AM2O3		2.53E-02		2.53E-02					
AS2O5		4.60E-08		4.60E-08					
B2O3		4.87E-06		4.87E-06					
B4O		5.59E-03		5.59E-03					
B2O		1.86E-08		1.86E-08					
BL2O3		2.82E-11		2.82E-11					
CaO		3.69E+02		3.69E+02					
ClO		1.38E-01		1.38E-01					
CR2O6		2.84E+02		2.84E+02					
CS2O		1.12E-02		1.12E-02					
CUO		1.13E-01		1.13E-01					
EU2O3		1.26E-03		1.26E-03					
FE2O3		1.03E+03		1.03E+03					
FORMER			7.78E+05						
H2O		1.30E-01		1.30E-01					
DMFAT									
K2O		1.74E+03		1.74E+03					
LA2O3		6.26E-02		6.26E-02					
M2O		4.14E-01		4.14E-01					
MNO2		3.80E+02		3.80E+02					
MCO3		1.03E+00		1.03E+00					
NA2O		1.61E+05		1.61E+05					
NI2O3		3.04E+02		3.04E+02					
NEO2		1.28E-02		1.28E-02					
OH-									
FeO5		2.69E+02		2.69E+02					
FeO2		1.83E+02		1.83E+02					
H+4									
FeO2		7.34E-02		7.34E-02					
SeO3		2.17E-05		2.17E-05					
SiO2		7.43E+01		7.43E+01					
SnO2		5.35E-11		5.35E-11					
SO3		7.31E+03		7.31E+03					
SOLIDS		9.85E-01		9.85E-01					
Sn+2									
SiO		5.17E-02		5.17E-02					
Ti2O7		8.44E+00		8.44E+00					
TiO2		3.21E-03		3.21E-03					
UC3		4.57E+02		4.57E+02					
W6		1.97E+00		1.97E+00					
ZnO		6.21E-01		6.21E-01					
ZrO2		2.79E-02		2.79E-02					

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Table B-20 Phase 1 LAW Mass Balance for Batch PC2/20 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	1.52E+06	1.52E+06	7.21E+03	1.69E+05	1.76E+05		1.52E+06	1.52E+06	7.27E+01	1.70E+03
Density (g/L)	1.32E+03	1.32E+03	1.32E+03	1.00E+03	1.01E+03		1.32E+03	1.32E+03	1.32E+03	1.00E+03
Total Mass Flow (kg)	2.00E+06	2.00E+06	9.49E+03	1.69E+05	1.79E+05		2.00E+06	2.00E+06	9.57E+01	1.70E+03
RADIONUCLIDES (Ci)										
Cesium	4.09E+05	4.07E+05	1.94E+03		1.94E+03		4.07E+05	4.07E+05	1.93E+01	
Strontium	1.01E+05	1.01E+05	4.78E+02		4.78E+02		1.19E+04	1.19E+04	5.71E-01	
Technetium	3.64E+02	3.62E+02	1.72E+00		1.72E+00		3.62E+02	3.62E+02	1.74E-02	
IU1	7.23E+02	7.19E+02	3.42E+00		3.42E+00		1.70E+02	1.70E+02	8.14E-03	
CHEMICALS (kg)										
AGP	1.33E-08	1.32E-08	6.30E-11		6.30E-11		1.32E-08	1.32E-08	6.33E-13	
AL(OH)4-	6.96E+03	6.92E+03	3.29E+01		3.29E+01		6.92E+03	6.92E+03	3.32E-01	
AM#3	2.00E-01	1.99E-01	9.43E-04		9.43E-04		4.69E-02	4.69E-02	2.23E-06	
AM#5	7.63E-09	7.61E-09	3.62E-11		3.62E-11		7.61E-09	7.61E-09	3.63E-13	
B#3	3.67E-07	3.65E-07	1.63E-09		1.63E-09		3.85E-07	3.85E-07	1.83E-11	
BE#2	3.36E-03	3.35E-03	1.60E-05		1.60E-05		1.36E-05	1.36E-05	5.16E-07	
BE#2	1.71E-09	1.70E-09	8.10E-12		8.10E-12		1.70E-09	1.70E-09	8.17E-14	
BI#3	6.45E-12	6.42E-12	3.05E-14		3.05E-14		6.42E-12	6.42E-12	3.03E-16	
C-14	2.93E-05	2.92E-05	1.40E-07		1.40E-07		2.93E-05	2.93E-05	1.41E-09	
CA#2	6.01E+02	5.98E+02	2.84E+00		2.84E+00		5.98E+02	5.98E+02	2.87E-02	
CM#2	5.18E-02	5.15E-02	2.45E-04		2.45E-04		5.15E-02	5.15E-02	2.47E-06	
CL-	3.42E+03	3.41E+03	1.62E+01		1.62E+01		3.41E+03	3.41E+03	1.63E-01	
CL2										
CO2										
CR#2	8.45E+04	8.41E+04	4.00E+02		4.00E+02		8.41E+04	8.41E+04	4.03E+00	
CR(OH)4-	6.01E+02	5.99E+02	2.83E+00		2.83E+00		5.99E+02	5.99E+02	2.87E-02	
CS#	4.73E+00	4.70E+00	2.24E-02		2.24E-02		4.70E+00	4.70E+00	2.26E-04	
CH#2	3.86E-02	3.86E-02	1.84E-04		1.84E-04		3.86E-02	3.86E-02	1.85E-06	
EU-154	7.37E-04	7.34E-04	3.49E-06		3.49E-06		7.34E-04	7.34E-04	3.52E-08	
F-	1.24E+02	1.23E+02	5.83E-01		5.83E-01		1.23E+02	1.23E+02	5.90E-03	
F2										
FE#3	1.63E+03	1.63E+03	7.73E+00	1.69E+05	7.73E+00		1.63E+03	1.63E+03	7.79E-02	
H2O	1.24E+06	1.24E+06	5.89E+03		5.89E+03		1.24E+06	1.24E+06	5.94E+01	1.70E+03
HE#2	5.18E-02	5.13E-02	2.43E-04		2.43E-04		5.13E-02	5.13E-02	2.47E-06	
K+	2.56E+03	2.56E+03	1.22E+01		1.22E+01		2.56E+03	2.56E+03	1.23E-01	
LA#3	3.61E-02	3.59E-02	1.71E-04		1.71E-04		3.59E-02	3.59E-02	1.72E-06	
MG#2	1.08E-01	1.08E-01	5.12E-04		5.12E-04		1.08E-01	1.08E-01	5.16E-06	
MH#4	5.46E+02	5.44E+02	2.59E+00		2.59E+00		5.44E+02	5.43E+02	2.61E-02	
MD#6	2.93E-01	2.92E-01	1.39E-03		1.39E-03		2.92E-01	2.92E-01	1.40E-05	
NA+	2.51E+05	2.50E+05	1.19E+03		1.19E+03		2.50E+05	2.50E+05	1.20E+01	
NI#3	4.91E+02	4.88E+02	2.32E+00		2.32E+00		4.88E+02	4.88E+02	2.34E-02	
NO2										
NO2-	5.82E+04	5.80E+04	2.76E+02		2.76E+02		5.80E+04	5.80E+04	2.78E+00	
NO3-	2.64E+05	2.62E+05	1.23E+03		1.23E+03		2.62E+05	2.62E+05	1.26E+01	
NE#4	7.52E-03	7.52E-03	3.58E-05		3.58E-05		7.52E-03	7.52E-03	3.60E-07	
O2										
OH-	2.05E+04	2.04E+04	9.70E+01		9.70E+01		2.04E+04	2.04E+04	9.77E-01	
EP#4	3.60E+02	3.59E+02	1.71E+00		1.71E+00		3.59E+02	3.59E+02	1.72E-02	
EO#-3	6.48E+02	6.45E+02	3.07E+00		3.07E+00		6.45E+02	6.45E+02	3.09E-02	
EU#4	5.26E-01	5.23E-01	2.49E-03		2.49E-03		1.24E-01	1.24E-01	5.94E-06	
SE#6	4.52E-06	4.52E-06	2.15E-08		2.15E-08		4.52E-06	4.52E-06	2.17E-10	
SI#4	2.30E+01	2.29E+01	1.09E-01		1.09E-01		2.29E+01	2.29E+01	1.10E-03	
SH#4	1.07E-11	1.07E-11	5.07E-14		5.07E-14		1.07E-11	1.07E-11	5.11E-16	
SO#-2	1.64E+04	1.63E+04	7.77E+01		7.77E+01		1.63E+04	1.63E+04	7.84E-01	
SR#2	7.27E-01	7.23E-01	3.44E-03		3.44E-03		8.56E-02	8.56E-02	4.11E-06	
TD#6	3.53E+01	3.51E+01	1.67E-01		1.67E-01		3.51E+01	3.51E+01	1.66E-03	
TI#4	6.50E-04	6.47E-04	3.08E-06		3.08E-06		6.47E-04	6.47E-04	3.10E-08	
TCL	4.69E+04	4.67E+04	2.22E+02		2.22E+02		4.67E+04	4.67E+04	2.24E+00	
UC#2	6.60E+02	6.57E+02	3.13E+00		3.13E+00		6.57E+02	6.57E+02	3.13E-02	
WH#6	6.73E-01	6.70E-01	3.19E-03		3.19E-03		6.70E-01	6.70E-01	3.21E-05	
ZH#2	2.05E-01	2.04E-01	9.70E-04		9.70E-04		2.04E-01	2.04E-01	9.77E-06	
ZR#4	6.94E-03	6.91E-03	3.29E-05		3.29E-05		6.91E-03	6.91E-03	3.31E-07	

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Table B-20 Phase 1 LAW Mass Balance for Batch PC2/20 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	2.00E+04	2.00E+02	1.98E+04		1.98E+04		2.02E+02	2.02E+00	2.00E+02	
RADIONUCLIDES (Ci)										
Cesium							8.86E+04	8.86E+02	8.77E+04	
Strontium										
Technetium							5.50E+02	5.50E+00	5.44E+02	
TU1										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM3							1.52E-01	1.52E-03	1.50E-01	
AM2O3										
AS2O5										
B2O3										
B4O										
BBO										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
ClO										
EU2O3										
FE2O3										
FORMER										
H2O										
LDHMT										
K2O										
LA2O3										
MCO										
MNO2										
MCO3										
NA2O										
NI2O3										
NFO2										
CH-							3.87E-01	3.87E-03	3.83E-01	
FO2										
FO2							3.99E-01	3.99E-03	3.95E-01	
FM4										
FU2										
SEO3										
SI02										
SN02										
SO3										
SOLIDS	2.00E+04	2.00E+02	1.98E+04		1.98E+04		2.00E+02	2.00E+00	1.98E+02	
SM+2							6.38E-01	6.38E-03	6.31E-01	
SNO										
TC2O7										
TiO2										
UC3										
WC3										
ZNO										
ZNO2										

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Table B-20 Phase 1 LAW Mass Balance for Batch PC2/20 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	1.76E+03	1.52E+06	1.32E+03		1.32E+03	1.52E+06	2.63E+06	1.33E+03	2.51E+03	3.84E+03
Density (g/L)	1.01E+03	1.32E+03	3.33E+03		3.33E+03	1.32E+03	1.00E+03	3.31E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)	1.80E+03	2.00E+06	4.38E+03		4.38E+03	2.00E+06	2.63E+06	4.39E+03	2.51E+03	6.90E+03
RADIONUCLIDES (Ci)										
Cesium	1.95E+01	1.92E+03	4.05E+05		4.05E+05	1.92E+03				
Strontium	5.71E-01	1.19E+04				1.19E+04				
Technetium	1.74E-02	3.59E+02	3.64E+00		3.64E+00	1.92E+02		1.67E+02		1.67E+02
IU1	8.14E-03	1.70E+02				1.70E+02				
CHEMICALS (kg)										
AG+	6.33E-13	1.32E-08				1.32E-08				
AL(OH)4-	3.32E-01	6.92E+03				6.92E+03				
AM+3	2.25E-06	4.69E-02				4.69E-02				
AS+5	3.65E-13	7.61E-09				7.61E-09				
BP+3	1.83E-11	3.83E-07				3.83E-07				
BS+2	1.63E-07	3.36E-03				3.36E-03				
BE+2	8.17E-14	1.70E-09				1.70E-09				
BI+3	3.08E-16	6.42E-12				6.42E-12				
C-14	1.41E-09	2.93E-05				2.93E-05				
CA+2	2.87E-02	5.98E+02				5.98E+02				
CD+2	2.47E-06	5.15E-02				5.15E-02				
CL-	1.63E-01	3.41E+03				3.41E+03				
CL2							3.41E+03			
CO2							2.33E+05			
CO3-2	4.03E+00	8.41E+04				8.41E+04				
CR(OH)4-	2.87E-02	5.98E+02				5.98E+02				
CSH	2.26E-04	2.21E-02	4.68E+00		4.68E+00	2.21E-02				
ClH2	1.85E-06	3.86E-02				3.86E-02				
EJ-154	3.52E-08	7.34E-04				7.34E-04				
F-	5.90E-03	1.23E+02				1.23E+02				
F2							1.23E+02			
FE+3	7.79E-02	1.63E+03				1.63E+03				
FD0	1.76E+03	1.24E+06				1.24E+06	1.25E+06		2.51E+03	2.51E+03
HG+2	2.47E-06	5.15E-02				5.15E-02				
It+	1.23E-01	2.56E+03				2.56E+03				
IA+3	1.72E-06	3.59E-02				3.59E-02				
IB+2	5.16E-06	1.03E-01				1.03E-01				
NI+4	2.61E-02	5.43E+02				5.43E+02				
MD+6	1.40E-05	2.92E-01				2.92E-01				
NA+	1.20E+01	2.50E+05	2.51E+03		2.51E+03	2.50E+05		2.51E+03		2.51E+03
NI+3	2.34E-02	4.88E+02				4.88E+02				
NO2							2.53E+05			
NO2-	2.78E+00	5.80E+04				5.80E+04				
NO3-	1.26E+01	2.62E+05				2.62E+05				
NE+4	3.60E-07	7.52E-03				7.52E-03				
O2							8.90E+05			
OH-	9.77E-01	2.04E+04	1.86E+03		1.86E+03	2.04E+04		1.86E+03		1.86E+03
FEH+4	1.72E-02	3.59E+02				3.59E+02				
FO4-3	3.09E-02	6.45E+02				6.45E+02				
FI+4	5.94E-06	1.24E-01				1.24E-01				
SE+6	2.17E-10	4.52E-06				4.52E-06				
SI+4	1.10E-03	2.29E+01				2.29E+01				
SN+4	5.11E-16	1.07E-11				1.07E-11				
SO4-2	7.84E-01	1.63E+04				1.63E+04				
SR+2	4.11E-06	8.56E-02				8.56E-02				
TIO4-	1.68E-03	3.47E+01	3.53E-01		3.53E-01	1.86E+01		1.62E+01		1.62E+01
TI+4	3.10E-08	6.47E-04				6.47E-04				
TCO	2.29E+00	4.67E+04				4.67E+04				
UDC+2	3.15E-02	6.57E+02				6.57E+02				
W+6	3.21E-05	6.70E-01				6.70E-01				
ZN+2	9.77E-06	2.04E-01				2.04E-01				
ZR+4	3.31E-07	6.91E-03				6.91E-03				

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Table B-20 Phase 1 LAW Mass Balance for Batch PC2/20 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	2.00E+02	2.02E+00		2.51E+03	2.51E+03	2.02E+00	3.65E+05			
RADIOISOTOPES (Ci)										
Cesium							1.92E+03			
Strontium	8.77E+04	8.86E+02				8.86E+02	1.28E+04			
Technetium							1.92E+02			
TU	5.44E+02	5.50E+00				5.50E+00	1.70E+02			
CHEMICALS (kg)										
AG2O							1.42E-08			
AL2O3							3.71E+03			
AMF3	1.50E-01	1.52E-03				1.52E-03				
AM2O3							5.32E-02			
AS2O5							1.17E-08			
B2O3							1.24E-06			
B4O							3.75E-03			
B6O							4.73E-09			
BL2O3							7.15E-12			
CaO							8.36E+02			
ClO							5.88E-02			
CR2O3							3.79E+02			
CS2O							2.34E-02			
ClO							4.83E-02			
EU2O3							8.49E-04			
FE2O3							2.32E+03			
FORMER										
HEO							5.56E-02			
DMAT				2.51E+03	2.51E+03					
K2O							3.09E+03			
LAGO3							4.22E-02			
MO							1.78E-01			
MNO2							8.60E+02			
MCO3							4.37E-01			
NA2O							3.37E+05			
NIL2O3							6.88E+02			
NFO2							8.53E-03			
OH-										
PCO5	3.83E-01	3.87E-03				3.87E-03	4.82E+02			
PCO2							4.14E+02			
PIH4	3.95E-01	3.99E-03				3.99E-03				
PUC2							1.45E-01			
SEO3							7.27E-06			
SIC2							4.89E+01			
SNO2							1.35E-11			
SO3							1.36E+04			
SOLIDS	1.98E+02	2.00E+00				2.00E+00	2.00E+00			
SR+2	6.31E-01	6.38E-03				6.38E-03				
SRO							1.08E-01			
TC2O7							1.77E+01			
TIC2							1.08E-03			
UE3							6.96E+02			
WC3							8.45E-01			
ZNO							2.54E-01			
ZNO2							9.33E-03			

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Table B-20 Phase 1 LAW Mass Balance for Batch PC2/20 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	2.63E+06				1.38E+06	1.25E+06	1.31E+03	1.31E+03	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	2.63E+06				1.38E+06	1.25E+06	4.38E+03	4.38E+03	1.00E+06

RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									

CHEMICALS (kg)									
AG+									
AL(OH)4-									
AN#3									
AS#5									
B#3									
BE#2									
BE#2									
BI#3									
C-14									
CA#2									
CD#2									
CL-									
CL2	3.41E+03				3.41E+03				
CO2	2.33E+05				2.33E+05				
CO3-2									
CR(OH)4-									
CS+									
CH2									
EU-154									
F-									
F2	1.23E+02				1.23E+02				
FE#3	1.25E+06					1.25E+06			
H2O									
HE#2									
K+									
LA#3									
MG#2									
MN#4									
MO#6									
NA+							2.51E+03	2.51E+03	
NI#3									
NO2	2.53E+05				2.53E+05				
NO2-									
NO3-									
NE#4									
O2	8.90E+05				8.90E+05				1.00E+06
OH-									
EP#4							1.86E+03	1.86E+03	
EO#-3									
EU#4									
SE#6									
SI#4									
SN#4									
SO#-2									
SR#2									
TOD#-									
TI#4									
TCC									
UD#2									
WH#6									
ZN#2									
ZR#4									

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Table B-20 Phase 1 LAW Mass Balance for Batch PC2/20 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		3.65E+05	1.63E+06	2.00E+06					
RADIONUCLIDES (Ci)									
Cesium		1.92E+03		1.92E+03					
Strontium		1.28E+04		1.28E+04					
Technetium		1.92E+02		1.92E+02					
Tb1		1.70E+02		1.70E+02					
CHEMICALS (kg)									
AC2O		1.42E-08		1.42E-08					
AL2O3		3.71E+03		3.71E+03					
AM3									
AM2O3		5.32E-02		5.32E-02					
AS2O5		1.17E-08		1.17E-08					
EGO3		1.24E-06		1.24E-06					
BAO		3.75E-03		3.75E-03					
BAO		4.73E-09		4.73E-09					
BI2O3		7.13E-12		7.13E-12					
CaO		8.36E+02		8.36E+02					
ClO		5.88E-02		5.88E-02					
CR2O3		3.79E+02		3.79E+02					
CS2O		2.34E-02		2.34E-02					
CUO		4.83E-02		4.83E-02					
EU2O3		8.49E-04		8.49E-04					
FE2O3		2.32E+03		2.32E+03					
FORMER			1.63E+06						
H2O		5.56E-02		5.56E-02					
IMHAT									
K2O		3.09E+03		3.09E+03					
LA2O3		4.22E-02		4.22E-02					
MCO		1.78E-01		1.78E-01					
MNO2		8.60E+02		8.60E+02					
MCO3		4.37E-01		4.37E-01					
Na2O		3.37E+05		3.37E+05					
NIL2O3		6.88E+02		6.88E+02					
NIC2O		8.53E-03		8.53E-03					
OH-									
P2O5		4.82E+02		4.82E+02					
SEO2		4.14E+02		4.14E+02					
EU+4									
FUO2		1.45E-01		1.45E-01					
SEO3		7.27E-06		7.27E-06					
SiO2		4.89E+01		4.89E+01					
SnO2		1.35E-11		1.35E-11					
SO3		1.36E+04		1.36E+04					
SOLIDS		2.00E+00		2.00E+00					
SR+2									
SrO		1.08E-01		1.08E-01					
TC2O7		1.77E+01		1.77E+01					
TiO2		1.08E-03		1.08E-03					
UD3		6.96E+02		6.96E+02					
UD3		8.45E-01		8.45E-01					
ZNO		2.54E-01		2.54E-01					
ZRO2		9.33E-03		9.33E-03					

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Table B-21 Phase 1 LAW Mass Balance for Batch PC2/21 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	2.97E+06	2.95E+06	1.40E+04	3.29E+05	3.43E+05		2.95E+06	2.95E+06	1.40E+02	3.30E+03
Density (g/L)	1.31E+03	1.31E+03	1.31E+03	1.00E+03	1.01E+03		1.31E+03	1.31E+03	1.31E+03	1.00E+03
Total Mass Flow (kg)	3.89E+06	3.88E+06	1.83E+04	3.29E+05	3.47E+05		3.88E+06	3.88E+06	1.84E+02	3.30E+03
RADIONUCLIDES (Ci)										
Cesium	4.94E+05	4.92E+05	2.33E+03		2.33E+03		4.92E+05	4.92E+05	2.33E+01	
Strontium	1.49E+05	1.48E+05	7.01E+02		7.01E+02		2.38E+04	2.38E+04	1.13E+00	
Technetium	5.81E+02	5.78E+02	2.73E+00		2.73E+00		5.78E+02	5.78E+02	2.74E-02	
IU	3.22E+02	3.21E+02	1.52E+00		1.52E+00		3.21E+02	3.21E+02	1.52E-02	
CHEMICALS (kg)										
AG+	1.25E-09	1.25E-09	5.90E-12		5.90E-12		1.25E-09	1.25E-09	5.92E-14	
AL(OH)4-	9.16E+04	9.12E+04	4.31E+02		4.31E+02		9.12E+04	9.12E+04	4.33E+00	
AM+3	5.52E-02	5.52E-02	2.61E-04		2.61E-04		5.52E-02	5.52E-02	2.62E-06	
AM+5	7.22E-10	7.19E-10	3.40E-12		3.40E-12		7.19E-10	7.19E-10	3.41E-14	
B+3	3.66E-08	3.64E-08	1.72E-10		1.72E-10		3.64E-08	3.6E-08	1.73E-12	
BE+2	3.83E-04	3.81E-04	1.93E-06		1.93E-06		3.81E-04	3.81E-04	1.93E-08	
BE+2	1.62E-10	1.61E-10	7.61E-13		7.61E-13		1.61E-10	1.61E-10	7.63E-15	
BI+3	6.09E-13	6.06E-13	2.87E-15		2.87E-15		6.06E-13	6.06E-13	2.88E-17	
C-14	7.11E-03	7.08E-03	3.35E-05		3.35E-05		7.08E-03	7.08E-03	3.36E-07	
CA+2	8.36E+02	8.32E+02	3.93E+00		3.93E+00		8.32E+02	8.32E+02	3.93E+02	
CD+2	5.52E-03	5.50E-03	2.60E-05		2.60E-05		5.50E-03	5.50E-03	2.61E-07	
CL-	7.16E+03	7.13E+03	3.37E+01		3.37E+01		7.13E+03	7.13E+03	3.38E-01	
CL2										
CO2										
CO3-2	1.26E+05	1.26E+05	5.94E+02		5.94E+02		1.26E+05	1.26E+05	5.96E+00	
CR(OH)4-	1.21E+03	1.20E+03	5.70E+00		5.70E+00		1.20E+03	1.20E+03	5.71E-02	
CS+	5.70E+00	5.68E+00	2.69E-02		2.69E-02		5.68E+00	5.68E+00	2.69E-04	
CH2	4.14E-03	4.12E-03	1.95E-05		1.95E-05		4.12E-03	4.12E-03	1.95E-07	
EU-154	5.30E-03	5.27E-03	2.49E-05		2.49E-05		5.27E-03	5.27E-03	2.50E-07	
F-	3.63E+03	3.61E+03	1.71E+01		1.71E+01		3.61E+03	3.61E+03	1.71E-01	
F2										
FE+3	1.98E+02	1.97E+02	9.32E-01	3.29E+05	9.32E-01		1.97E+02	1.97E+02	9.33E-03	
HD2	2.49E+06	2.48E+06	1.17E+04		3.41E+05		2.48E+06	2.48E+06	1.18E+02	3.30E+03
HG+2	5.52E-03	5.50E-03	2.60E-05		2.60E-05		5.50E-03	5.50E-03	2.61E-07	
K+	7.07E+03	7.03E+03	3.33E+01		3.33E+01		7.03E+03	7.03E+03	3.34E-01	
LA+3	4.08E-03	4.06E-03	1.92E-05		1.92E-05		4.06E-03	4.06E-03	1.93E-07	
LN+2	1.16E-02	1.15E-02	5.45E-05		5.45E-05		1.15E-02	1.15E-02	5.47E-07	
MH+4	6.60E+01	6.57E+01	3.11E-01		3.11E-01		6.57E+01	6.57E+01	3.12E-03	
ND+6	3.12E-02	3.10E-02	1.47E-04		1.47E-04		3.10E-02	3.10E-02	1.47E-06	
Na+	4.92E+05	4.89E+05	2.32E+03		2.32E+03		4.89E+05	4.89E+05	2.32E+01	
NI+3	6.69E+02	6.66E+02	3.15E+00		3.15E+00		6.66E+02	6.66E+02	3.16E-02	
NO2										
NO2-	1.52E+05	1.51E+05	7.16E+02		7.16E+02		1.51E+05	1.51E+05	7.18E+00	
NO3-	4.15E+05	4.13E+05	1.95E+03		1.95E+03		4.13E+05	4.13E+05	1.96E+01	
NH4+	8.53E-04	8.49E-04	4.02E-06		4.02E-06		8.49E-04	8.49E-04	4.03E-08	
O2										
OH-	2.10E+04	2.09E+04	9.89E+01		9.89E+01		2.09E+04	2.09E+04	9.92E-01	
FBH4	4.36E+01	4.34E+01	2.05E-01		2.05E-01		4.34E+01	4.34E+01	2.06E-03	
FO4-3	8.62E+03	8.58E+03	4.06E+01		4.06E+01		8.58E+03	8.58E+03	4.07E-01	
FU+4	1.82E+00	1.81E+00	8.57E-03		8.57E-03		1.81E+00	1.81E+00	8.60E-05	
SE+6	4.62E-07	4.60E-07	2.18E-09		2.18E-09		4.60E-07	4.60E-07	2.18E-11	
SI+4	2.59E+00	2.58E+00	1.22E-02		1.22E-02		2.58E+00	2.58E+00	1.22E-04	
SN+4	1.01E-12	1.01E-12	4.76E-15		4.76E-15		1.01E-12	1.01E-12	4.77E-17	
SO4-2	2.49E+04	2.47E+04	1.27E+02		1.27E+02		2.47E+04	2.47E+04	1.27E+00	
SR+2	1.07E+00	1.07E+00	5.04E-03		5.04E-03		1.07E+00	1.07E+00	5.05E-05	
TCO4-	5.63E+01	5.60E+01	2.65E-01		2.65E-01		5.60E+01	5.60E+01	2.66E-03	
TI+4	6.61E-05	6.58E-05	3.11E-07		3.11E-07		6.58E-05	6.58E-05	3.12E-09	
TOC	5.12E+04	5.09E+04	2.41E+02		2.41E+02		5.09E+04	5.09E+04	2.42E+00	
UD2+2	7.88E+01	7.84E+01	3.71E-01		3.71E-01		7.84E+01	7.84E+01	3.72E-03	
WH6	7.18E-02	7.15E-02	3.38E-04		3.38E-04		7.15E-02	7.15E-02	3.39E-06	
ZN+2	2.17E-02	2.16E-02	1.02E-04		1.02E-04		2.16E-02	2.16E-02	1.02E-06	
ZR+4	7.06E-04	7.03E-04	3.32E-06		3.32E-06		7.03E-04	7.03E-04	3.33E-08	

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Table B-21 Phase 1 LAW Mass Balance for Batch PC2/21 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	3.90E+04	3.90E+02	3.86E+04		3.86E+04		3.91E+02	3.91E+00	3.87E+02	
RADIONUCLIDES (Ci)										
Cesium							1.25E+05	1.25E+03	1.23E+05	
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
BBO										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
HO										
EMFAT										
K2O										
LA2O3										
MO										
MNO2										
MCO3										
NA2O										
NI2O3										
NIO2										
OH-							3.38E-01	3.38E-03	3.35E-01	
PO25										
FE02										
FL02										
SE03										
SI02										
SNO2										
SO3										
SOLIDS	3.90E+04	3.90E+02	3.86E+04		3.86E+04		3.90E+02	3.90E+00	3.86E+02	
SR+2							8.95E-01	8.95E-03	8.87E-01	
SRO										
TIC2O7										
TIC02										
UD3										
W03										
ZNO										
ZNO2										

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Table B-21 Phase 1 IAW Mass Balance for Batch PC2/21 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	3.44E+03	2.95E+06	2.57E+03		2.57E+03	2.95E+06	4.13E+06	2.58E+03	4.91E+03	7.50E+03
Density (g/L)	1.01E+03	1.31E+03	3.38E+03		3.38E+03	1.31E+03	1.00E+03	3.32E+03	1.00E+03	1.80E+03
Total Mass Flow (kg)	3.48E+03	3.88E+06	8.56E+03		8.56E+03	3.88E+06	4.13E+06	8.57E+03	4.91E+03	1.33E+04
RADIONUCLIDES (Ci)										
Cesium	2.33E+01	3.73E+03	4.88E+05		4.88E+05	3.73E+03				
Strontium	1.13E+00	2.38E+04				2.38E+04				
Technetium	2.74E-02	5.72E+02	5.81E+00		5.81E+00	3.75E+02		1.97E+02		1.97E+02
I-131	1.52E-02	3.21E+02				3.21E+02				
CHEMICALS (kg)										
A0+	5.92E-14	1.25E-09				1.25E-09				
AL(OH)4-	4.33E+00	9.12E+04				9.12E+04				
AM+3	2.62E-06	5.52E-02				5.52E-02				
AS+5	3.41E-14	7.19E-10				7.19E-10				
BA+3	1.73E-12	3.64E-08				3.64E-08				
BA+2	1.81E-08	3.81E-04				3.81E-04				
BE+2	7.63E-15	1.61E-10				1.61E-10				
BI+3	2.88E-17	6.06E-13				6.06E-13				
C-14	3.36E-07	7.08E-03				7.08E-03				
CA+2	3.95E-02	8.32E+02				8.32E+02				
CD+2	2.61E-07	5.50E-03				5.50E-03				
CL-	3.38E-01	7.13E+03				7.13E+03				
CL2							7.13E+03			
CO2							2.79E+05			
CO3-2	5.96E+00	1.26E+05				1.26E+05				
CR(OH)4-	5.71E-02	1.20E+03				1.20E+03				
CS+	2.69E-04	4.33E-02	5.63E+00		5.63E+00	4.33E-02				
CU+2	1.96E-07	4.12E-03				4.12E-03				
EJ-154	2.50E-07	5.27E-03				5.27E-03				
F-	1.71E-01	3.61E+03				3.61E+03				
F2							3.61E+03			
FE+3	9.35E-03	1.97E+02				1.97E+02				
H2O	3.42E+03	2.48E+06				2.48E+06	2.52E+06		4.91E+03	4.91E+03
HE+2	2.61E-07	5.50E-03				5.50E-03				
HF	3.84E-01	7.03E+03				7.03E+03				
LA+3	1.93E-07	4.06E-03				4.06E-03				
MD+2	5.47E-07	1.15E-02				1.15E-02				
MN+4	3.12E-03	6.57E+01				6.57E+01				
MD+6	1.47E-06	3.10E-02				3.10E-02				
NA+	2.32E+01	4.89E+05	4.92E+03		4.92E+03	4.89E+05		4.92E+03		4.92E+03
NI+3	3.16E-02	6.66E+02				6.66E+02				
NO2							4.58E+05			
NO2-	7.18E+00	1.51E+05				1.51E+05				
NO3-	1.96E+01	4.13E+05				4.13E+05				
NH4+	4.03E-08	8.49E-04				8.49E-04				
O2							8.56E+05			
OH-	9.92E-01	2.09E+04	3.64E+03		3.64E+03	2.09E+04		3.64E+03		3.64E+03
FBH4	2.06E-03	4.34E+01				4.34E+01				
FO4-3	4.07E-01	8.58E+03				8.58E+03				
FU+4	8.60E-05	1.81E+00				1.81E+00				
SE+6	2.18E-11	4.60E-07				4.60E-07				
SI+4	1.22E-04	2.58E+00				2.58E+00				
SH+4	4.77E-17	1.01E-12				1.01E-12				
SO4-2	1.27E+00	2.67E+04				2.67E+04				
SR+2	8.11E-06	1.71E-01				1.71E-01				
TCO4-	2.66E-03	5.54E+01	5.63E-01		5.63E-01	5.54E+01		1.91E+01		1.91E+01
TI+4	3.12E-09	6.58E-05				6.58E-05				
ICC	2.42E+00	5.09E+04				5.09E+04				
UCO+2	3.72E-03	7.84E+01				7.84E+01				
WH6	3.39E-06	7.15E-02				7.15E-02				
ZH+2	1.02E-06	2.16E-02				2.16E-02				
ZH+4	3.33E-08	7.03E-04				7.03E-04				

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Table B-21 Phase 1 LAW Mass Balance for Batch PC2/21 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	3.87E+02	3.91E+00		4.92E+03	4.92E+03	3.91E+00	7.49E+05			
RADIONUCLIDES (Ci)										
Cesium										
Strontium	1.23E+05	1.25E+03				1.25E+03	3.75E+03			
Technetium							2.50E+04			
TU							3.75E+02			
							3.19E+02			
CHEMICALS (kg)										
AGSO							1.34E-09			
AL2O3							4.89E+04			
AMG08							6.07E-02			
ASZ05							1.10E-09			
B2O3							1.17E-07			
BAO							4.25E-04			
BE0							4.46E-10			
Bi2O3							6.76E-13			
CaO							1.16E+03			
ClO							6.28E-03			
CR2O3							7.62E+02			
CS2O							4.58E-02			
ClO							5.16E-03			
EU2O3							6.10E-03			
FE2O3							2.82E+02			
FORMER										
HE0							5.93E-03			
DMAT										
K2O				4.92E+03	4.92E+03		8.47E+03			
La2O3							4.76E-03			
MO							1.91E-02			
MNO2							1.04E+02			
MCO3							4.66E-02			
Na2O							6.60E+05			
Ni2O3							9.38E+02			
NiCO2							9.63E-04			
OH-										
PCO5	3.35E-01	3.38E-03				3.38E-03	6.41E+03			
PCO2							5.01E+01			
PUO2							2.05E+00			
SE03							7.40E-07			
STO2							5.52E+00			
SNO2							1.28E-12			
SO3							2.23E+04			
SOLIDS	3.86E+02	3.90E+00				3.90E+00	3.90E+00			
SR+2	8.87E-01	8.95E-03				8.95E-03				
SRO							2.12E-01			
TC2O7							3.45E+01			
TI02							1.10E-04			
UO3							8.30E+01			
VO3							9.01E-02			
ZNO							2.69E-02			
ZrO2							9.49E-04			

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Table B-21 Phase 1 LAW Mass Balance for Batch FC2/21 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.13E+06				1.60E+06	2.52E+06	2.56E+03	2.56E+03	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	4.13E+06				1.60E+06	2.52E+06	8.56E+03	8.56E+03	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
B+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	7.13E+03				7.13E+03				
CO2	2.79E+05				2.79E+05				
CO3-2									
CR(OH)4-									
CS+									
Cl+2									
EU-154									
F-									
F2	3.61E+03				3.61E+03				
FE+3						2.52E+06			
H2O	2.52E+06								
H3+2									
K+									
LA+3									
MA+2									
MA+4									
MD+6									
NA+							4.92E+03	4.92E+03	
NI+3									
NO2	4.58E+05				4.58E+05				
NO2-									
NO3-									
NE+4									
O2	8.56E+05				8.56E+05				1.00E+06
OH-									
FB+4							3.64E+03	3.64E+03	
FO4-3									
FU+4									
SE+6									
SI+4									
SN+4									
SO4-2									
SR+2									
TDO4-									
TI+4									
TIC									
UC+2									
W+6									
ZN+2									
ZR+4									

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Table B-21 Phase 1 LAW Mass Balance for Batch PC2/21 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		7.49E+05	3.16E+06	3.91E+06					
RADIONUCLIDES (Cl)									
Cesium		3.75E+03		3.75E+03					
Strontium		2.50E+04		2.50E+04					
Technetium		3.75E+02		3.75E+02					
TRU		3.19E+02		3.19E+02					
CHEMICALS (kg)									
AC2O		1.34E-09		1.34E-09					
AL2O3		4.89E+04		4.89E+04					
AM2O5		6.07E-02		6.07E-02					
AS2O5		1.10E-09		1.10E-09					
B2O3		1.17E-07		1.17E-07					
BAD		4.25E-04		4.25E-04					
BBD		4.46E-10		4.46E-10					
BL2O3		6.76E-13		6.76E-13					
CaO		1.16E+03		1.16E+03					
ClO		6.28E-03		6.28E-03					
CR2O3		7.62E+02		7.62E+02					
CS2O		4.58E-02		4.58E-02					
ClO		5.16E-03		5.16E-03					
EU2O3		6.10E-03		6.10E-03					
FE2O3		2.82E+02		2.82E+02					
FORMER			3.16E+06						
HEO		5.93E-03		5.93E-03					
IMMAT									
K2O		8.47E+03		8.47E+03					
LA2O3		4.76E-03		4.76E-03					
MO		1.91E-02		1.91E-02					
MNO2		1.04E+02		1.04E+02					
MCO3		4.66E-02		4.66E-02					
NA2O		6.60E+05		6.60E+05					
NI2O3		9.38E+02		9.38E+02					
NFC2		9.63E-04		9.63E-04					
CH-									
PCO5		6.41E+03		6.41E+03					
PCO2		5.01E+01		5.01E+01					
PIR2		2.05E+00		2.05E+00					
SEO3		7.40E-07		7.40E-07					
STO2		5.52E+00		5.52E+00					
SNO2		1.28E-12		1.28E-12					
SO6		2.23E+04		2.23E+04					
SOLIDS		3.90E+00		3.90E+00					
SR+2									
SRO		2.12E-01		2.12E-01					
TC2O7		3.45E+01		3.45E+01					
TiO2		1.10E-04		1.10E-04					
UO3		8.30E+01		8.30E+01					
VO3		9.01E-02		9.01E-02					
ZNO		2.69E-02		2.69E-02					
ZRC2		9.49E-04		9.49E-04					

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Table B-22 Phase 1 LAW Mass Balance for Batch PC2/22 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.67E+06	3.65E+06	1.72E+04	3.91E+05	4.08E+05		3.65E+06	3.65E+06		
Density (g/L)	1.26E+03	1.26E+03	1.26E+03	1.00E+03	1.01E+03		1.26E+03	1.26E+03		
Total Mass Flow (kg)	4.63E+06	4.61E+06	2.17E+04	3.91E+05	4.13E+05		4.61E+06	4.61E+06		
RADIONUCLIDES (Ci)										
Cesium	3.12E+04	3.11E+04	1.46E+02		1.46E+02		3.11E+04	3.11E+04		
Strontium	9.32E+03	9.28E+03	4.37E+01		4.37E+01		9.28E+03	9.28E+03		
Technetium	3.66E+01	3.64E+01	1.72E-01		1.72E-01		3.64E+01	3.64E+01		
TU	1.92E+01	1.91E+01	9.00E-02		9.00E-02		1.91E+01	1.91E+01		
CHEMICALS (kg)										
AG+	1.78E-01	1.77E-01	8.35E-04		8.35E-04		1.77E-01	1.77E-01		
AL(OH)4-	1.12E+05	1.11E+05	5.23E+02		5.23E+02		1.11E+05	1.11E+05		
AM+3	3.15E-03	3.14E-03	1.48E-05		1.48E-05		3.14E-03	3.14E-03		
AS+5	9.33E-02	9.29E-02	4.39E-04		4.39E-04		9.29E-02	9.29E-02		
BA+3	1.57E-09	1.57E-09	7.37E-12		7.37E-12		1.57E-09	1.57E-09		
BA+2	8.39E-02	8.35E-02	3.93E-04		3.93E-04		8.35E-02	8.35E-02		
BE+2	6.96E-12	6.93E-12	3.27E-14		3.27E-14		6.93E-12	6.93E-12		
BI+3	2.96E-01	2.94E-01	1.39E-03		1.39E-03		2.94E-01	2.94E-01		
C-14	4.53E-04	4.53E-04	2.14E-06		2.14E-06		4.53E-04	4.53E-04		
CA+2	5.24E+01	5.22E+01	2.46E-01		2.46E-01		5.22E+01	5.22E+01		
CD+2	2.07E-01	2.06E-01	9.68E-04		9.68E-04		2.06E-01	2.06E-01		
CL-	4.73E+02	4.73E+02	2.23E+00		2.23E+00		4.73E+02	4.73E+02		
CL2										
CO2										
CO3-2	9.59E+04	9.59E+04	4.50E+02		4.50E+02		9.59E+04	9.59E+04		
CR(OH)4-	8.10E+01	8.06E+01	3.80E-01		3.80E-01		8.06E+01	8.06E+01		
CS+	3.60E-01	3.59E-01	1.69E-03		1.69E-03		3.59E-01	3.59E-01		
CU+2	7.82E-03	7.78E-03	3.67E-05		3.67E-05		7.78E-03	7.78E-03		
EU-154	3.38E-04	3.36E-04	1.58E-06		1.58E-06		3.36E-04	3.36E-04		
F-	4.66E+03	4.64E+03	2.18E+01		2.18E+01		4.64E+03	4.64E+03		
F2										
FE+3	1.21E+01	1.20E+01	5.67E-02	3.91E+05	5.67E-02		1.20E+01	1.20E+01		
HO2	3.07E+06	3.05E+06	1.44E+04		1.44E+04		3.05E+06	3.05E+06		
HO+2	7.23E-04	7.20E-04	3.39E-06		3.39E-06		7.20E-04	7.20E-04		
K+	4.40E+02	4.47E+02	2.11E+00		2.11E+00		4.47E+02	4.47E+02		
LA+3	1.90E-04	1.89E-04	8.91E-07		8.91E-07		1.89E-04	1.89E-04		
MD+2	3.81E-01	3.79E-01	1.79E-03		1.79E-03		3.79E-01	3.79E-01		
MN+4	3.51E+00	3.49E+00	1.65E-02		1.65E-02		3.49E+00	3.49E+00		
MO+6	1.37E-01	1.37E-01	6.44E-04		6.44E-04		1.37E-01	1.37E-01		
NA+	5.87E+05	5.84E+05	2.75E+03		2.75E+03		5.84E+05	5.84E+05		
NI+3	4.18E+01	4.16E+01	1.96E-01		1.96E-01		4.16E+01	4.16E+01		
NO2										
NO2-	1.86E+05	1.85E+05	8.71E+02		8.71E+02		1.85E+05	1.85E+05		
NO3-	4.51E+05	4.49E+05	2.12E+03		2.12E+03		4.49E+05	4.49E+05		
NO+4	3.97E-05	3.95E-05	1.86E-07		1.86E-07		3.96E-05	3.96E-05		
O2										
OH-	1.63E+04	1.63E+04	7.66E+01		7.66E+01		1.63E+04	1.63E+04		
PO4-3	3.02E+00	3.00E+00	1.41E-02		1.41E-02		3.00E+00	3.00E+00		
PO4-3	1.17E+04	1.16E+04	5.47E+01		5.47E+01		1.16E+04	1.16E+04		
PU+4	1.16E-01	1.15E-01	5.41E-04		5.41E-04		1.15E-01	1.15E-01		
SE+6	5.64E-04	5.62E-04	2.65E-06		2.65E-06		5.62E-04	5.62E-04		
SI+4	1.21E-01	1.20E-01	5.67E-04		5.67E-04		1.20E-01	1.20E-01		
SO4-2	1.88E+04	1.88E+04	8.83E+01		8.83E+01		1.88E+04	1.88E+04		
SR+2	6.71E-02	6.67E-02	3.14E-04		3.14E-04		6.67E-02	6.67E-02		
TD+4	3.54E+00	3.53E+00	1.65E-02		1.65E-02		3.53E+00	3.53E+00		
TI+4	7.15E-03	7.11E-03	3.35E-05		3.35E-05		7.11E-03	7.11E-03		
TCC	8.36E+04	8.32E+04	3.92E+02		3.92E+02		8.32E+04	8.32E+04		
UO2+2	4.06E+00	4.04E+00	1.91E-02		1.91E-02		4.04E+00	4.04E+00		
WH6	3.27E-03	3.25E-03	1.53E-05		1.53E-05		3.25E-03	3.25E-03		
ZN+2	3.70E+00	3.68E+00	1.73E-02		1.73E-02		3.68E+00	3.68E+00		
ZR+4	5.67E-02	5.64E-02	2.66E-04		2.66E-04		5.64E-02	5.64E-02		

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Table B-22 Phase 1 LAW Mass Balance for Batch PC2/22 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.63E+04	4.63E+02	4.59E+04		4.59E+04		4.63E+02	4.63E+02		
RADIONUCLIDES (Cl.)										
Cesium										
Strontium										
Technetium										
TRU										
CHEMICALS (kg)										
ACG0										
AL2O3										
AMG03										
AS2O5										
B2O3										
B4O										
BHO										
BL2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
EL2O3										
FE2O3										
FORMER										
H2O										
IMHAT										
K2O										
LA2O3										
MG										
MIC2										
MOB										
NA2O										
NIL2O3										
NEO2										
FE2O5										
FRG2										
FLU2										
SEB3										
STO2										
SO3										
SOLIDS	4.63E+04	4.63E+02	4.59E+04		4.59E+04		4.63E+02	4.63E+02		
SRO										
TC2O7										
TIO2										
UD3										
WOB										
ZNO										
ZRO2										

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Table B-22 Phase 1 LAW Mass Balance for Batch PC2/22 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)		3.65E+06	3.06E+03		3.06E+03	3.65E+06	4.74E+06		1.00E-09	1.00E-09
Density (g/L)		1.26E+03	3.34E+03		3.34E+03	1.26E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)		4.61E+06	1.02E+04		1.02E+04	4.61E+06	4.74E+06		1.00E-09	1.00E-09
RADIONUCLIDES (Ci)										
Cesium		4.48E+03	2.66E+04		2.66E+04	4.48E+03				
Strontium		9.22E+03				9.22E+03				
Technetium		3.60E+01	3.66E-01		3.66E-01	3.60E+01				
I-131		1.91E+01				1.91E+01				
CHEMICALS (kg)										
AG+		1.77E-01				1.77E-01				
AL(OH)4-		1.11E+05				1.11E+05				
AM+3		3.14E-03				3.14E-03				
ASH+5		9.22E-02				9.22E-02				
B+3		1.57E-09				1.57E-09				
BA+2		8.35E-02				8.35E-02				
BE+2		6.93E-12				6.93E-12				
BI+3		2.94E-01				2.94E-01				
C-14		4.53E-04				4.53E-04				
CA+2		5.22E+01				5.22E+01				
CD+2		2.06E-01				2.06E-01				
CL-		4.73E+02				4.73E+02				
CL2							4.73E+02			
CO2								3.75E+05		
CO3-2		9.53E+04				9.53E+04				
CR(OH)4-		8.06E+01				8.06E+01				
CS+		5.17E-02	3.07E-01		3.07E-01	5.17E-02				
Cl+2		7.78E-03				7.78E-03				
EU-154		3.36E-04				3.36E-04				
F-		4.64E+03				4.64E+03				
F2							4.64E+03			
FE+3		1.20E+01				1.20E+01				
H2O		3.05E+06				3.05E+06	3.10E+06		1.00E-09	1.00E-09
H3P+2		7.20E-04				7.20E-04				
HS-		4.47E+02				4.47E+02				
IA+3		1.89E-04				1.89E-04				
MG+2		3.79E-01				3.79E-01				
MP+4		3.49E+00				3.49E+00				
ND+6		1.37E-01				1.37E-01				
NA+		5.84E+05	5.87E+03		5.87E+03	5.84E+05				
NI+3		4.16E+01				4.16E+01				
NO2							5.18E+05			
NO2-		1.85E+05				1.85E+05				
NO3-		4.49E+05				4.49E+05				
NO3-		3.96E-05				3.96E-05				
O2							7.40E+05			
OH-		1.63E+04	4.34E+03		4.34E+03	1.63E+04				
EP+4		3.00E+00				3.00E+00				
FO4-3		1.16E+04				1.16E+04				
FU+4		1.15E-01				1.15E-01				
SE+6		5.62E-04				5.62E-04				
SI+4		1.20E-01				1.20E-01				
SO4-2		1.88E+04				1.88E+04				
SR+2		6.67E-02				6.67E-02				
TIO4-		3.49E+00				3.49E+00				
TI+4		7.11E-03	3.54E-02		3.54E-02	7.11E-03				
TIC		8.32E+04				8.32E+04				
UD2+2		4.04E+00				4.04E+00				
WH+6		3.25E-03				3.25E-03				
ZN+2		3.68E+00				3.68E+00				
ZR+4		5.64E-02				5.64E-02				

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Table B-22 Phase 1 LAW Mass Balance for Batch PC2/22 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)		4.63E+02		5.87E+03	5.87E+03	4.63E+02	8.72E+05			
RADIONUCLIDES (CL)										
Cesium							4.48E+03			
Strontium							9.28E+03			
Technetium							3.60E+01			
TU							1.90E+01			
CHEMICALS (kg)										
AC2O							1.90E-01			
AL2O3							5.95E+04			
AN2O3							3.45E-03			
AS2O5							1.43E-01			
B2O3							5.04E-09			
B4O							9.32E-02			
B2O							1.92E-11			
BL2O3							3.28E-01			
CaO							7.30E+01			
CO							2.35E-01			
CR2O3							5.10E+01			
CS2O							5.47E-02			
CU							9.74E-03			
EU2O3							3.89E-04			
FE2O3							1.72E+01			
FURMER										
H2O							7.77E-04			
HMAT										
K2O				5.87E+03	5.87E+03					
LA2O3							5.39E+02			
Li3							2.22E-04			
MO2							6.29E-01			
MO3							5.53E+00			
Na2O							2.05E-01			
NL2O3							7.87E+05			
NL2O							5.86E+01			
NF2							4.49E-05			
FO5							8.68E+03			
FIG2							3.47E+00			
FUC2							1.30E-01			
SE2O							9.03E-04			
STO2							2.58E-01			
ST3							1.56E+04			
SOLIDS		4.63E+02				4.63E+02				
SRO							4.63E+02			
SRO							7.86E-02			
TIC2O7							3.32E+00			
TIC2							1.19E-02			
UC3							4.28E+00			
UC3							4.10E-03			
ZNO							4.58E+00			
ZFC2							7.62E-02			

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Table B-22 Phase 1 LAW Mass Balance for Batch PC2/22 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.74E+06				1.64E+06	3.10E+06	3.06E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	4.74E+06				1.64E+06	3.10E+06	1.02E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TsU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AM+3									
AS+5									
B+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	4.73E+02				4.73E+02				
CO2	3.75E+05				3.75E+05				
CO3--2									
CR(OH)4-									
CS+									
CH2									
EU-154									
F-									
F2	4.64E+03				4.64E+03				
FE+3									
H2O	3.10E+06					3.10E+06			
HO+2									
K+									
LA+3									
MD+2									
MO+4									
ND+6									
NA+							5.87E+03	5.75E-10	
NI+3									
NO2	5.18E+05				5.18E+05				
NO2-									
NO3-									
NO+4									
O2	7.40E+05				7.40E+05				1.00E+06
OH-									
OH+4							4.34E+03	4.25E-10	
EO4-3									
EUH4									
SE+6									
SI+4									
SO4--2									
SR+2									
TCO4-									
TI+4									
TCC									
UC2+2									
WH6									
ZN+2									
ZR+4									

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Table B-22 Phase 1 LAW Mass Balance for Batch FC2/22 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		8.72E+05	3.79E+06	4.66E+06					
RADIONUCLIDES (Ci)									
Cesium		4.48E+03		4.48E+03					
Strontium		9.22E+03		9.22E+03					
Technetium		3.60E+01		3.60E+01					
TbU		1.90E+01		1.90E+01					
CHEMICALS (kg)									
AC2O		1.90E-01		1.90E-01					
AL2O3		5.95E+04		5.95E+04					
AM2O3		3.45E-03		3.45E-03					
AS2O5		1.43E-01		1.43E-01					
B2O3		5.04E-09		5.04E-09					
B4O		9.32E-02		9.32E-02					
B8O		1.92E-11		1.92E-11					
BL2O3		3.22E-01		3.22E-01					
CaO		7.30E+01		7.30E+01					
ClO		2.35E-01		2.35E-01					
CR2O3		5.10E+01		5.10E+01					
CS2O		5.47E-02		5.47E-02					
CUO		9.74E-03		9.74E-03					
EU2O3		3.89E-04		3.89E-04					
FE2O3		1.72E+01		1.72E+01					
FORMER			3.79E+06	3.79E+06					
HEO		7.77E-04		7.77E-04					
HMAT									
K2O		5.39E+02		5.39E+02					
LA2O3		2.22E-04		2.22E-04					
MO		6.29E-01		6.29E-01					
MNO2		5.53E+00		5.53E+00					
MCO3		2.05E-01		2.05E-01					
NA2O		7.87E+05		7.87E+05					
NIL2O3		5.86E+01		5.86E+01					
NEO2		4.49E-05		4.49E-05					
PCO5		8.68E+03		8.68E+03					
PEO2		3.47E+00		3.47E+00					
PLO2		1.30E-01		1.30E-01					
SEO3		9.03E-04		9.03E-04					
STO2		2.58E-01		2.58E-01					
SO3		1.56E+04		1.56E+04					
SOLIDS		4.63E+02		4.63E+02					
SPO		7.86E-02		7.86E-02					
TC2O7		3.32E+00		3.32E+00					
TIO2		1.19E-02		1.19E-02					
UO3		4.22E+00		4.22E+00					
VO3		4.10E-03		4.10E-03					
ZNO		4.58E+00		4.58E+00					
ZNO2		7.62E-02		7.62E-02					

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Table B-23 Phase 1 LAW Mass Balance for Batch PC2/23 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	3.59E+06	3.57E+06	1.68E+04	3.84E+05	4.01E+05		3.57E+06	3.57E+06	1.68E+02	3.84E+03
Density (g/L)	1.27E+03	1.27E+03	1.27E+03	1.00E+03	1.01E+03		1.27E+03	1.27E+03	1.27E+03	1.00E+03
Total Mass Flow (kg)	4.55E+06	4.52E+06	2.13E+04	3.84E+05	4.05E+05		4.52E+06	4.52E+06	2.13E+02	3.84E+03
RADIONUCLIDES (Cl)										
Cesium	8.01E+04	7.97E+04	3.75E+02		3.75E+02		7.97E+04	7.97E+04	3.75E+00	
Strontium	8.74E+04	8.70E+04	4.10E+02		4.10E+02		8.70E+04	8.70E+04	4.10E+00	
Technetium	1.43E+02	1.42E+02	6.69E-01		6.69E-01		1.42E+02	1.42E+02	6.69E-03	
TsU	1.93E+01	1.92E+01	9.02E-02		9.02E-02		1.92E+01	1.92E+01	9.02E-04	
CHEMICALS (kg)										
Ag+	2.24E-02	2.23E-02	1.03E-04		1.05E-04		2.23E-02	2.23E-02	1.03E-06	
Al(OH) ₃	1.08E+05	1.08E+05	5.06E+02		5.06E+02		1.08E+05	1.08E+05	5.06E+00	
Am ³⁺	3.97E-03	3.96E-03	1.62E-05		1.62E-05		3.96E-03	3.96E-03	1.62E-07	
As ⁵⁺	8.90E-02	8.86E-02	4.17E-04		4.17E-04		8.86E-02	8.86E-02	4.17E-06	
B ³⁺	1.97E+00	1.96E+00	9.23E-03		9.23E-03		1.96E+00	1.96E+00	9.23E-05	
BA ²⁺	2.69E+00	2.67E+00	1.26E-02		1.26E-02		2.67E+00	2.67E+00	1.26E-04	
BE ²⁺	2.34E-13	2.33E-13	1.10E-15		1.10E-15		2.33E-13	2.33E-13	1.10E-17	
BI ³⁺	1.57E-02	1.57E-02	7.37E-05		7.37E-05		1.57E-02	1.57E-02	7.37E-07	
C-14	2.27E-05	2.26E-05	1.06E-07		1.06E-07		2.26E-05	2.26E-05	1.06E-09	
Ca ²⁺	1.04E+02	1.03E+02	4.86E-01		4.86E-01		1.03E+02	1.03E+02	4.86E-03	
CD ²⁺	1.74E-01	1.73E-01	8.14E-04		8.14E-04		1.73E-01	1.73E-01	8.14E-06	
Cl ⁻	4.42E+02	4.39E+02	2.07E+00		2.07E+00		4.39E+02	4.39E+02	2.07E-02	
Cl ₂										
CO ₂										
CO ₃ ²⁻	9.50E+04	9.46E+04	4.45E+02		4.45E+02		9.46E+04	9.46E+04	4.45E+00	
CR(OH) ₃	7.66E+01	7.63E+01	3.59E-01		3.59E-01		7.63E+01	7.63E+01	3.59E-03	
CS ⁺	9.25E-01	9.20E-01	4.33E-03		4.33E-03		9.20E-01	9.20E-01	4.33E-05	
CU ²⁺	4.13E-04	4.11E-04	1.94E-06		1.94E-06		4.11E-04	4.11E-04	1.94E-08	
EU-154	1.35E-05	1.34E-05	6.31E-08		6.31E-08		1.34E-05	1.34E-05	6.31E-10	
F ⁻	4.55E+03	4.53E+03	2.13E+01		2.13E+01		4.53E+03	4.53E+03	2.13E-01	
F ₂										
FE ³⁺	5.63E+00	5.60E+00	2.64E-02		2.64E-02		5.60E+00	5.60E+00	2.64E-04	
H ₂ O	3.00E+06	2.98E+06	1.40E+04	3.84E+05	3.98E+05		2.98E+06	2.98E+06	1.40E+02	3.84E+03
HS ²⁻	3.39E-05	3.37E-05	1.59E-07		1.59E-07		3.37E-05	3.37E-05	1.59E-09	
K ⁺	3.14E+03	3.12E+03	1.47E+01		1.47E+01		3.12E+03	3.12E+03	1.47E-01	
LA ³⁺	2.78E+01	2.77E+01	1.30E-01		1.30E-01		2.77E+01	2.77E+01	1.30E-03	
MD ²⁺	6.94E+00	6.91E+00	3.25E-02		3.25E-02		6.91E+00	6.91E+00	3.25E-04	
MN ⁴⁺	1.31E-01	1.30E-01	6.11E-04		6.11E-04		1.30E-01	1.30E-01	6.11E-06	
MO ⁶⁺	2.24E-02	2.23E-02	1.05E-04		1.05E-04		2.23E-02	2.23E-02	1.05E-06	
Na ⁺	5.76E+05	5.74E+05	2.70E+03		2.70E+03		5.74E+05	5.74E+05	2.70E+01	
NI ³⁺	3.10E+01	3.09E+01	1.45E-01		1.45E-01		3.09E+01	3.09E+01	1.45E-03	
NiO ₂										
NiO ₂	1.79E+05	1.78E+05	8.38E+02		8.38E+02		1.78E+05	1.78E+05	8.38E+00	
NO ₃ ⁻	4.47E+05	4.43E+05	2.09E+03		2.09E+03		4.43E+05	4.43E+05	2.09E+01	
Ni ⁴⁺	1.39E-06	1.39E-06	6.52E-09		6.52E-09		1.39E-06	1.39E-06	6.52E-11	
O ₂										
OH ⁻	2.26E+04	2.25E+04	1.06E+02		1.06E+02		2.25E+04	2.25E+04	1.06E+00	
PB ⁴⁺	6.37E-01	6.34E-01	2.98E-03		2.98E-03		6.34E-01	6.34E-01	2.98E-05	
PO ₄ ³⁻	1.12E+04	1.11E+04	5.22E+01		5.22E+01		1.11E+04	1.11E+04	5.22E-01	
FU ⁴⁺	7.75E-02	7.71E-02	3.63E-04		3.63E-04		7.71E-02	7.71E-02	3.63E-06	
SE ⁶⁺	1.31E-02	1.30E-02	6.11E-05		6.11E-05		1.30E-02	1.30E-02	6.11E-07	
SI ⁴⁺	1.48E+01	1.47E+01	6.92E-02		6.92E-02		1.47E+01	1.47E+01	6.92E-04	
SO ₄ ²⁻	1.94E+04	1.94E+04	9.11E+01		9.11E+01		1.94E+04	1.94E+04	9.11E-01	
SR ²⁺	6.29E-01	6.26E-01	2.95E-03		2.95E-03		2.07E-01	2.07E-01	9.79E-06	
TCO ₄ ⁻	1.38E+01	1.38E+01	6.48E-02		6.48E-02		1.38E+01	1.38E+01	6.48E-04	
TI ⁴⁺	3.81E-04	3.79E-04	1.79E-06		1.79E-06		3.79E-04	3.79E-04	1.79E-08	
TCC	8.04E+04	8.00E+04	3.76E+02		3.76E+02		8.00E+04	8.00E+04	3.76E+00	
UC ₂ H ₂	2.28E+01	2.27E+01	1.07E-01		1.07E-01		2.27E+01	2.26E+01	1.07E-03	
WH ⁶	1.13E-04	1.13E-04	5.30E-07		5.30E-07		1.13E-04	1.13E-04	5.30E-09	
ZH ²⁺	1.05E+01	1.05E+01	4.94E-02		4.94E-02		1.05E+01	1.05E+01	4.94E-04	
Zr ⁴⁺	3.02E-03	3.01E-03	1.42E-05		1.42E-05		3.01E-03	3.01E-03	1.42E-07	

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Table B-23 Phase 1 LAW Mass Balance for Batch PC2/23 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	4.55E+04	4.53E+02	4.50E+04		4.50E+04		4.53E+02	4.55E+00	4.51E+02	
RADIONUCLIDES (Cl)										
Cesium							5.83E+04	5.83E+02	5.77E+04	
Strontium										
Technetium										
TU										
CHEMICALS (kg)										
AC2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O										
B4O										
B2O3										
CaO										
ClO										
CR2O3										
CS2O										
CUO										
EU2O3										
FE2O3										
FORMER										
H2O										
IMMAT										
K2O										
LA2O3										
MO										
MO2										
MO3										
NA2O										
NI2O3										
NI2O										
OH-							1.59E-01	1.59E-03	1.57E-01	
PO25										
PR2O										
RU2O										
SE2O										
SI2O										
SO3										
SOLIDS	4.55E+04	4.53E+02	4.50E+04		4.50E+04		4.53E+02	4.55E+00	4.50E+02	
SR+2							4.19E-01	4.19E-03	4.15E-01	
SRO										
TC2O7										
TIO2										
UO3										
VO3										
ZNO										
ZNCO										

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Table B-23 Phase 1 LAW Mass Balance for Batch PC2/23 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	4.01E+03	3.57E+06	3.01E+03		3.01E+03	3.57E+06	4.66E+06		1.00E-09	1.00E-09
Density (g/L)	1.01E+03	1.27E+03	3.34E+03		3.34E+03	1.27E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)	4.05E+03	4.52E+06	1.00E+04		1.00E+04	4.52E+06	4.66E+06		1.00E-09	1.00E-09
RADIONUCLIDES (Ci)										
Cesium	3.75E+00	4.40E+03	7.53E+04		7.53E+04	4.40E+03				
Strontium	1.33E+00	2.87E+04				2.87E+04				
Technetium	6.69E-03	1.41E+02	1.43E+00		1.43E+00	1.41E+02				
Iru	9.02E-04	1.92E+01				1.92E+01				
CHEMICALS (kg)										
AC+	1.05E-06	2.23E-02				2.23E-02				
AL(OH)4-	5.06E+00	1.08E+05				1.08E+05				
AM+3	1.86E-07	3.96E-03				3.96E-03				
ASH+5	4.17E-06	8.86E-02				8.86E-02				
B+3	9.23E-05	1.96E+00				1.96E+00				
BA+2	1.26E-04	2.67E+00				2.67E+00				
BE+2	1.10E-17	2.33E-13				2.33E-13				
BI+3	7.37E-07	1.57E-02				1.57E-02				
C-14	1.06E-09	2.26E-05				2.26E-05				
CA+2	4.86E-03	1.03E+02				1.03E+02				
CD+2	8.14E-06	1.73E-01				1.73E-01				
CL-	2.07E-02	4.39E+02				4.39E+02				
CL2										
Cl2										
Cl3-2	4.45E+00	9.46E+04				9.46E+04				
CR(OH)4-	3.59E-03	7.63E+01				7.63E+01				
CS+	4.33E-05	5.08E-02	8.69E-01		8.69E-01	5.08E-02				
CU+2	1.94E-08	4.11E-04				4.11E-04				
EU-154	6.31E-10	1.34E-05				1.34E-05				
F-	2.13E-01	4.53E+03				4.53E+03				
F2										
FE+3	2.64E-04	5.60E+00				5.60E+00				
HD2	3.98E+03	2.98E+06				2.98E+06				
HE+2	1.59E-09	3.37E-05				3.37E-05				
H+	1.47E-01	3.12E+03				3.12E+03				
LA+3	1.30E-03	2.77E+01				2.77E+01				
MG+2	3.25E-04	6.91E+00				6.91E+00				
MN+4	6.11E-06	1.30E-01				1.30E-01				
MD+6	1.05E-06	2.23E-02				2.23E-02				
NA+	2.70E+01	5.74E+05	5.76E+03		5.76E+03	5.74E+05				
NI+3	1.45E-03	3.09E+01				3.09E+01				
NO2										
NCO2	8.38E+00	1.78E+05				1.78E+05				
NO3-	2.09E+01	4.43E+05				4.43E+05				
NO+4	6.52E-11	1.38E-06				1.38E-06				
O2										
OH-	1.06E+00	2.25E+04	4.27E+03		4.27E+03	2.25E+04				
EB+4	2.98E-05	6.34E-01				6.34E-01				
EO4-3	5.22E-01	1.11E+04				1.11E+04				
FU+4	3.63E-06	7.71E-02				7.71E-02				
SE+6	6.11E-07	1.30E-02				1.30E-02				
SI+4	6.92E-04	1.47E+01				1.47E+01				
SD+2	9.11E-01	1.94E+04				1.94E+04				
SE+2	9.73E-06	2.07E-01				2.07E-01				
TCD4-	6.48E-04	1.36E+01	1.38E-01		1.38E-01	1.36E+01				
TI+4	1.79E-08	3.79E-04				3.79E-04				
TCC	3.76E+00	8.00E+04				8.00E+04				
UD2+2	1.07E-03	2.26E+01				2.26E+01				
W+6	5.30E-09	1.13E-04				1.13E-04				
ZN+2	4.94E-04	1.03E+01				1.03E+01				
ZR+4	1.42E-07	3.01E-03				3.01E-03				

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Table B-23 Phase 1 LAW Mass Balance for Batch PC2/23 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	4.51E+02	4.55E+00		5.76E+03	5.76E+03	4.55E+00	8.59E+05			
RADIONUCLIDES (Ci)										
Cesium							4.40E+03			
Strontium	5.77E+04	5.83E+02				5.83E+02	2.93E+04			
Technetium							1.41E+02			
TU							1.91E+01			
CHEMICALS (kg)										
AC2O							2.39E-02			
AL2O3							5.77E+04			
AM2O3							4.35E-03			
AS2O5							1.36E-01			
B2O3							6.31E+00			
B4O							2.99E+00			
B2O							6.47E-13			
BL2O3							1.75E-02			
CaO							1.44E+02			
ClO							1.97E-01			
CR2O3							4.83E+01			
CS2O							5.37E-02			
CU							5.15E-04			
EU2O3							1.55E-05			
FE2O3							8.00E+00			
FORMER										
H2O				5.76E+03	5.76E+03		3.64E-05			
DMFMT										
K2O							3.76E+03			
LA2O3							3.25E+01			
MO							1.15E+01			
MNO2							2.06E-01			
MO3							3.34E-02			
Na2O							7.73E+05			
NI2O3							4.35E+01			
NFO2							1.57E-06			
NFO2	1.57E-01	1.59E-03				1.59E-03				
OH-							8.29E+03			
FSO5							7.32E-01			
FR02							8.75E-02			
FUC2							2.09E-02			
SBO3							3.15E+01			
SIO2							1.61E+04			
SO3							4.53E+00			
SOLIDS	4.50E+02	4.55E+00				4.55E+00				
SR+2	4.15E-01	4.19E-03				4.19E-03				
SFO							2.48E-01			
TU2O7							1.30E+01			
TIO2							6.33E-04			
UD3							2.40E+01			
UD3							1.42E-04			
ZNO							1.31E+01			
ZNO2							4.07E-03			

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Table B-23 Phase 1 LAW Mass Balance for Batch PC2/23 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	4.66E+06				1.63E+06	3.04E+06	3.01E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)									
	4.66E+06				1.63E+06	3.04E+06	1.00E+04	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TRU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AP+3									
AS+5									
B+3									
BA+2									
BE+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	4.39E+02				4.39E+02				
CL2	3.62E+05				3.62E+05				
CO3-2									
CR(OH)4-									
CS+									
CU+2									
EU-154									
F-									
F2	4.53E+03				4.53E+03				
FE+3						3.04E+06			
H2O	3.04E+06								
HE+2									
K+									
LA+3									
MD+2									
MN+4									
MO+6									
NA+							5.76E+03	5.75E-10	
NI+3									
NO2	5.08E+05				5.08E+05				
NO2-									
NO3-									
NE+4									
O2	7.52E+05				7.52E+05				1.00E+06
OH-									
EBH4							4.27E+03	4.25E-10	
FO4-3									
FU+4									
SE+6									
SI+4									
SO4-2									
SR+2									
TDO+									
TI+4									
TOC									
UO2+2									
W+6									
ZN+2									
ZR+4									

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Table B-23 Phase 1 LAW Mass Balance for Batch PC2/23 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		6.59E+05	3.72E+06	4.58E+06					
RADIONUCLIDES (Ci)									
Cesium		4.40E+03		4.40E+03					
Strontium		2.93E+04		2.93E+04					
Technetium		1.41E+02		1.41E+02					
TbU		1.91E+01		1.91E+01					
CHEMICALS (kg)									
AC2O		2.39E-02		2.39E-02					
AL2O3		5.77E+04		5.77E+04					
AM2O5		4.35E-03		4.35E-03					
AS2O5		1.36E-01		1.36E-01					
B2O3		6.31E+00		6.31E+00					
BAD		2.99E+00		2.99E+00					
BB		6.47E-13		6.47E-13					
BL2O3		1.73E-02		1.73E-02					
CaO		1.44E+02		1.44E+02					
ClO		1.97E-01		1.97E-01					
CR2O3		4.83E+01		4.83E+01					
CS2O		5.37E-02		5.37E-02					
CUO		5.15E-04		5.15E-04					
EU2O3		1.55E-05		1.55E-05					
FE2O3		8.00E+00		8.00E+00					
FORMER			3.72E+06	3.72E+06					
H2O		3.64E-05		3.64E-05					
IMMAT									
K2O		3.76E+03		3.76E+03					
LA2O3		3.25E+01		3.25E+01					
M2O		1.15E+01		1.15E+01					
MNO2		2.06E-01		2.06E-01					
MOO3		3.34E-02		3.34E-02					
Na2O		7.73E+05		7.73E+05					
NIL2O3		4.35E+01		4.35E+01					
NEO2		1.57E-06		1.57E-06					
OH-									
PO5		8.29E+03		8.29E+03					
PKO2		7.32E-01		7.32E-01					
H2O2		8.75E-02		8.75E-02					
SEF8		2.09E-02		2.09E-02					
SiO2		3.15E+01		3.15E+01					
SO3		1.61E+04		1.61E+04					
SOLIDS		4.55E+00		4.55E+00					
SR+2									
SrO		2.48E-01		2.48E-01					
Ti2O7		1.50E+01		1.50E+01					
TiO2		6.33E-04		6.33E-04					
UO3		2.40E+01		2.40E+01					
VO3		1.42E-04		1.42E-04					
ZNO		1.31E+01		1.31E+01					
ZrO2		4.07E-03		4.07E-03					

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Table B-24 Phase 1 LAW Mass Balance for Batch PC2/24 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Volume (L)	1.79E+06	1.78E+06	8.40E+03	1.92E+05	2.00E+05		1.78E+06	1.78E+06	8.40E+01	1.92E+03
Density (g/L)	1.27E+03	1.27E+03	1.27E+03	1.00E+03	1.01E+03		1.27E+03	1.27E+03	1.27E+03	1.00E+03
Total Mass Flow (kg)	2.27E+06	2.26E+06	1.06E+04	1.92E+05	2.03E+05		2.26E+06	2.26E+06	1.06E+02	1.92E+03
RADIONUCLIDES (Ci)										
Cesium	4.17E+04	4.15E+04	1.96E+02		1.96E+02		4.15E+04	4.15E+04	1.96E+00	
Strontium	4.58E+04	4.53E+04	2.15E+02		2.15E+02		4.43E+04	4.43E+04	6.73E-01	
Technetium	7.45E+01	7.41E+01	3.50E-01		3.50E-01		7.41E+01	7.41E+01	3.50E-03	
TRU	9.76E+00	9.71E+00	4.58E-02		4.58E-02		9.71E+00	9.71E+00	4.58E-04	
CHEMICALS (kg)										
AG+	7.14E-03	7.10E-03	3.35E-05		3.35E-05		7.10E-03	7.10E-03	3.35E-07	
AL(OH)4-	5.39E+04	5.37E+04	2.53E+02		2.53E+02		5.37E+04	5.37E+04	2.53E+00	
#H+3	2.03E-03	2.02E-03	9.53E-06		9.53E-06		2.02E-03	2.02E-03	9.53E-08	
AS+5	4.42E-02	4.40E-02	2.08E-04		2.08E-04		4.40E-02	4.40E-02	2.08E-06	
B#0	1.04E+00	1.03E+00	4.84E-03		4.84E-03		1.03E+00	1.03E+00	4.84E-05	
BA+2	1.41E+00	1.40E+00	6.61E-03		6.61E-03		1.40E+00	1.40E+00	6.61E-05	
BI+3	6.19E-04	6.16E-04	2.90E-06		2.90E-06		6.16E-04	6.16E-04	2.90E-08	
C-14	3.00E-06	2.98E-06	1.41E-08		1.41E-08		2.98E-06	2.98E-06	1.41E-10	
CM+2	5.34E+01	5.31E+01	2.51E-01		2.51E-01		5.31E+01	5.31E+01	2.51E-03	
CM+2	8.62E-02	8.58E-02	4.05E-04		4.05E-04		8.58E-02	8.58E-02	4.05E-06	
CL-	2.23E+02	2.22E+02	1.05E+00		1.05E+00		2.22E+02	2.22E+02	1.05E-02	
CL2										
CL2										
CO3-2	4.74E+04	4.71E+04	2.22E+02		2.22E+02		4.71E+04	4.71E+04	2.22E+00	
CR(OH)4-	3.87E+01	3.85E+01	1.82E-01		1.82E-01		3.85E+01	3.85E+01	1.82E-03	
CS+	4.81E-01	4.79E-01	2.26E-03		2.26E-03		4.79E-01	4.79E-01	2.26E-05	
CI#2	1.62E-05	1.62E-05	7.62E-08		7.62E-08		1.62E-05	1.62E-05	7.62E-10	
EU-154	4.73E-07	4.70E-07	2.22E-09		2.22E-09		4.70E-07	4.70E-07	2.22E-11	
F-	2.28E+03	2.27E+03	1.07E+01		1.07E+01		2.27E+03	2.27E+03	1.07E-01	
F2										
FE+3	2.72E+00	2.71E+00	1.28E-02	1.92E+05	1.28E-02		2.71E+00	2.71E+00	1.28E-04	1.92E+03
H2O	1.50E+06	1.49E+06	7.01E+03		1.49E+06		1.49E+06	1.49E+06	7.01E+01	
H#+2	1.27E-06	1.26E-06	5.96E-09		5.96E-09		1.26E-06	1.26E-06	5.96E-11	
K+	1.64E+03	1.63E+03	7.70E+00		7.70E+00		1.63E+03	1.63E+03	7.70E-02	
LA#3	1.47E+01	1.46E+01	6.89E-02		6.89E-02		1.46E+01	1.46E+01	6.89E-04	
MD+2	3.64E+00	3.62E+00	1.71E-02		1.71E-02		3.62E+00	3.62E+00	1.71E-04	
MN+4	4.46E-03	4.44E-03	2.09E-05		2.09E-05		4.44E-03	4.44E-03	2.09E-07	
MO+6	8.22E-03	8.18E-03	3.86E-05		3.86E-05		8.18E-03	8.18E-03	3.86E-07	
NA+	2.88E+05	2.86E+05	1.35E+03		1.35E+03		2.86E+05	2.86E+05	1.35E+01	
NI+3	1.56E+01	1.55E+01	7.30E-02		7.30E-02		1.55E+01	1.55E+01	7.30E-04	
NO2										
NO2-	8.99E+04	8.94E+04	4.22E+02		4.22E+02		8.94E+04	8.94E+04	4.22E+00	
NO3-	2.24E+05	2.23E+05	1.05E+03		1.05E+03		2.23E+05	2.23E+05	1.05E+01	
NO#4	4.55E-08	4.52E-08	2.13E-10		2.13E-10		4.52E-08	4.52E-08	2.13E-12	
O2										
OH-	1.15E+04	1.14E+04	5.39E+01		5.39E+01		1.14E+04	1.14E+04	5.39E-01	
PH+4	2.74E-01	2.73E-01	1.29E-03		1.29E-03		2.73E-01	2.73E-01	1.29E-05	
PO4-3	5.57E+03	5.55E+03	2.61E+01		2.61E+01		5.55E+03	5.55E+03	2.61E-01	
PU+4	3.83E-02	3.83E-02	1.81E-04		1.81E-04		3.83E-02	3.83E-02	1.81E-06	
SE#6	6.83E-03	6.80E-03	3.21E-05		3.21E-05		6.80E-03	6.80E-03	3.21E-07	
SI+4	7.79E+00	7.75E+00	3.63E-02		3.63E-02		7.75E+00	7.75E+00	3.63E-04	
SO4-2	9.76E+03	9.72E+03	4.58E+01		4.58E+01		9.72E+03	9.72E+03	4.58E-01	
SR+2	3.29E-01	3.28E-01	1.54E-03		1.54E-03		1.03E-01	1.03E-01	4.86E-06	
TD#4	7.21E+00	7.18E+00	3.39E-02		3.39E-02		7.18E+00	7.18E+00	3.39E-04	
TI+4	1.50E-05	1.49E-05	7.01E-08		7.01E-08		1.49E-05	1.49E-05	7.01E-10	
TICL	4.01E+04	3.99E+04	1.88E+02		1.88E+02		3.99E+04	3.99E+04	1.88E+00	
UO2#2	1.19E+01	1.18E+01	5.58E-02		5.58E-02		1.18E+01	1.18E+01	5.58E-04	
W#6	3.67E-06	3.66E-06	1.72E-08		1.72E-08		3.66E-06	3.66E-06	1.72E-10	
ZM+2	5.47E+00	5.44E+00	2.57E-02		2.57E-02		5.44E+00	5.44E+00	2.57E-04	
ZR#4	1.18E-04	1.18E-04	5.52E-07		5.52E-07		1.18E-04	1.18E-04	5.52E-09	

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Table B-24 Phase 1 LAW Mass Balance for Batch PC2/24 (6 sheets)

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (kg)	2.27E+04	2.27E+02	2.25E+04		2.25E+04		2.28E+02	2.28E+00	2.25E+02	
RADIONUCLIDES (Cl)										
Cesium Strontium Technetium TRI							3.12E+04	3.12E+02	3.09E+04	
CHEMICALS (kg)										
AS2O										
AL2O3										
AM2O3										
AS2O5										
B2O3										
B4O7										
BIL2O3										
CaO										
ClO										
CR2O3										
CS2O										
ClO										
EU2O3										
FE2O3										
FORMER										
H2O										
DMPT										
K2O										
LA2O3										
MO										
MO2										
MO3										
Na2O										
NIL2O3										
NEO2										
CH-							8.49E-02	8.49E-04	8.41E-02	
FO2										
FR2										
FR2										
SE2										
STO2										
SO3										
SOLIDS	2.27E+04	2.27E+02	2.25E+04		2.25E+04		2.27E+02	2.27E+00	2.25E+02	
SR+2							2.25E-01	2.25E-03	2.22E-01	
SRO										
TC2O7										
TIO2										
UO3										
W2O3										
ZNO										
ZRO2										

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Table B-24 Phase 1 LAW Mass Balance for Batch PC2/24 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
LIQUID COMPONENTS										
Volume (L)	2.01E+03	1.78E+06	1.50E+03		1.50E+03	1.78E+06	2.83E+06		1.00E-09	1.00E-09
Density (g/L)	1.01E+03	1.27E+03	3.34E+03		3.34E+03	1.27E+03	1.00E+03		1.00E+03	1.00E+03
Total Mass Flow (kg)	2.03E+03	2.26E+06	5.01E+03		5.01E+03	2.26E+06	2.83E+06		1.00E-09	1.00E-09

RADIONUCLIDES (Ci)										
Cesium	1.96E+00	2.20E+03	3.93E+04		3.93E+04	2.20E+03				
Strontium	6.73E-01	1.43E+04				1.43E+04				
Technetium	3.50E-03	7.34E+01	7.45E-01		7.45E-01	7.34E+01				
TU1	4.58E-04	9.71E+00				9.71E+00				

CHEMICALS (kg)										
AG+	3.33E-07	7.10E-03				7.10E-03				
AL(OH)4-	2.53E+00	5.37E+04				5.37E+04				
AM#3	9.53E-08	2.02E-03				2.02E-03				
AS#5	2.08E-06	4.40E-02				4.40E-02				
PH#3	4.86E-05	1.03E+00				1.03E+00				
BA#2	6.61E-05	1.44E+00				1.44E+00				
BE#3	2.90E-08	6.16E-04				6.16E-04				
C-14	1.41E-10	2.98E-06				2.98E-06				
CA#2	2.51E-03	5.31E+01				5.31E+01				
CD#2	4.05E-06	8.58E-02				8.58E-02				
CL-	1.03E-02	2.22E+02				2.22E+02				
CL2							2.22E+02			
CO2							1.81E+05			
CO3-2	2.22E+00	4.71E+04				4.71E+04				
CR(OH)4-	1.82E-03	3.85E+01				3.85E+01				
CS+	2.26E-05	2.53E-02	4.54E-01		4.54E-01	2.53E-02				
CH#2	7.62E-10	1.62E-05				1.62E-05				
EU-154	2.22E-11	3.70E-07				3.70E-07				
F-	1.07E-01	2.27E+03				2.27E+03				
F2							2.27E+03			
FE#3	1.28E-04	2.71E+00				2.71E+00				
H2O	1.99E+03	1.49E+06				1.49E+06	1.51E+06		1.00E-09	1.00E-09
HE#2	5.96E-11	1.26E-06				1.26E-06				
K+	7.70E-02	1.63E+03				1.63E+03				
LA#3	6.89E-04	1.46E+01				1.46E+01				
M#2	1.71E-04	3.62E+00				3.62E+00				
MN#4	2.09E-07	4.44E-03				4.44E-03				
MD#6	3.86E-07	8.18E-03				8.18E-03				
NI#1	1.35E+01	2.86E+05	2.88E+03		2.88E+03	2.86E+05				
NI#3	7.30E-04	1.52E+01				1.52E+01				
NO2							2.55E+05			
NO2-	4.22E+00	8.94E+04				8.94E+04				
NO3-	1.05E+01	2.23E+05				2.23E+05				
NE#4	2.13E-12	4.52E-08				4.52E-08				
O2							8.77E+05			
OH-	5.39E-01	1.14E+04	2.13E+03		2.13E+03	1.14E+04				
FB#4	1.29E-05	2.73E-01				2.73E-01				
FO#3	2.61E-01	5.53E+03				5.53E+03				
FI#4	1.81E-06	3.83E-02				3.83E-02				
SE#6	3.21E-07	6.80E-03				6.80E-03				
SI#4	3.65E-04	7.75E+00				7.75E+00				
SO4-2	4.58E-01	9.72E+03				9.72E+03				
SR#2	4.86E-06	1.03E-01				1.03E-01				
TDO#4	3.39E-04	7.11E+00	7.21E-02		7.21E-02	7.11E+00				
TI#4	7.01E-10	1.49E-05				1.49E-05				
TCC	1.88E+00	3.99E+04				3.99E+04				
UC#2	5.58E-04	1.18E+01				1.18E+01				
W#6	1.72E-10	3.68E-06				3.68E-06				
ZN#2	2.57E-04	5.44E+00				5.44E+00				
ZR#4	5.55E-09	1.18E-04				1.18E-04				

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Table B-24 Phase 1 LAW Mass Balance for Batch PC2/24 (6 sheets)

STREAM NAME	11	12	13	14	15	16	16A	17	18	19
SOLID COMPONENTS										
Total Mass Flow (kg)	2.25E+02	2.22E+00		2.88E+03	2.88E+03	2.22E+00	4.29E+05			
RADIONUCLIDES (Ci)										
Cesium							2.20E+03			
Strontium	3.09E+04	3.12E+02				3.12E+02	1.46E+04			
Technetium							7.34E+01			
TRU							9.68E+00			
CHEMICALS (kg)										
AG2O							7.63E-03			
AL2O3							2.88E+04			
AM2O3							2.22E-03			
AS2O3							6.75E-02			
B2O3							3.32E+00			
BAO							1.57E+00			
BI2O3							6.86E-04			
CaO							7.44E+01			
ClO							9.83E-02			
CR2O3							2.44E+01			
CS2O							2.68E-02			
ClO							2.02E-05			
EU2O3							5.45E-07			
FE2O3							3.87E+00			
FURMER										
HEO							1.37E-06			
DMAT				2.88E+03	2.88E+03					
K2O							1.97E+03			
LA2O3							1.71E+01			
M2O							6.00E+00			
M2O2							7.02E-03			
MO3							1.23E-02			
Na2O							3.86E+05			
NI2O3							2.18E+01			
NFO2							5.13E-08			
CF-	8.41E-02	8.49E-04				8.49E-04				
P2O5							4.15E+03			
PHO2							3.15E-01			
P2O2							4.33E-02			
SEO3							1.05E-02			
SiO2							1.66E+01			
SO3							8.10E+03			
SOLIDS	2.25E+02	2.27E+00				2.27E+00	2.27E+00			
SR+2	2.22E-01	2.25E-03				2.25E-03				
SFO							1.24E-01			
TC2O7							6.76E+00			
TiO2							2.48E-05			
UC3							1.23E+01			
UC3							4.61E-06			
ZNO							6.78E+00			
ZK02							1.59E-04			

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Table B-24 Phase 1 LAW Mass Balance for Batch PC2/24 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
LIQUID COMPONENTS									
Volume (L)	2.83E+06				1.32E+06	1.51E+06	1.50E+03	3.00E-10	1.00E+06
Density (g/L)	1.00E+03				1.00E+03	1.00E+03	3.34E+03	3.34E+03	1.00E+03
Total Mass Flow (kg)	2.83E+06				1.32E+06	1.51E+06	5.01E+03	1.00E-09	1.00E+06
RADIONUCLIDES (Ci)									
Cesium									
Strontium									
Technetium									
TU									
CHEMICALS (kg)									
AG+									
AL(OH)4-									
AP+3									
AS+5									
B+3									
BA+2									
BI+3									
C-14									
CA+2									
CD+2									
CL-									
CL2	2.22E+02				2.22E+02				
CO2	1.81E+05				1.81E+05				
CO3-2									
CR(OH)4-									
CS+									
CI+2									
EU-154									
F-									
F2	2.27E+03				2.27E+03				
FE+3									
H2O	1.51E+06					1.51E+06			
HO+2									
K+									
LA+3									
MG+2									
MO+4									
MO+6									
NA+									
NI+3									
NO2	2.55E+05				2.55E+05			2.88E+03	5.75E-10
NO2-									
NO3-									
NE+4									
O2	8.77E+05				8.77E+05				1.00E+06
OH-									
PH+4									
PO4-3									
RU+4									
SE+6									
SI+4									
SO4-2									
SR+2									
TOD4-									
Ti+4									
TiO2									
UO2+2									
W+6									
ZH+2									
ZR+4									

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Table B-24 Phase 1 LAW Mass Balance for Batch PC2/24 (6 sheets)

STREAM NAME	20	21	22	23	24	25	26	27	28
SOLID COMPONENTS									
Total Mass Flow (kg)		4.29E+05	1.86E+06	2.29E+06					
RADIONUCLIDES (Cl)									
Cesium		2.20E+03		2.20E+03					
Strontium		1.46E+04		1.46E+04					
Technetium		7.34E+01		7.34E+01					
TRU		9.68E+00		9.68E+00					
CHEMICALS (kg)									
ACG0		7.63E-03		7.63E-03					
AL2O3		2.88E+04		2.88E+04					
AM2O3		2.22E-03		2.22E-03					
AS2O5		6.75E-02		6.75E-02					
B2O3		3.32E+00		3.32E+00					
B4O		1.57E+00		1.57E+00					
BL2O3		6.86E-04		6.86E-04					
CaO		7.44E+01		7.44E+01					
ClO		9.80E-02		9.80E-02					
CR2O3		2.44E+01		2.44E+01					
CS2O		2.68E-02		2.68E-02					
ClO		2.02E-05		2.02E-05					
EU2O3		5.45E-07		5.45E-07					
FE2O3		3.87E+00		3.87E+00					
FURMER			1.86E+06						
H2O		1.37E-06		1.37E-06					
IDMAT									
Na2O		1.97E+03		1.97E+03					
LAG2O3		1.71E+01		1.71E+01					
Na2O		6.00E+00		6.00E+00					
NH4E		7.02E-03		7.02E-03					
NaCl		1.23E-02		1.23E-02					
Na2O		3.86E+05		3.86E+05					
Ni2O3		2.18E+01		2.18E+01					
NFC2		5.13E-08		5.13E-08					
OH-									
Fe2O5		4.15E+03		4.15E+03					
FeO2		3.15E-01		3.15E-01					
HUO2		4.33E-02		4.33E-02					
SiO3		1.09E-02		1.09E-02					
SiO2		1.66E+01		1.66E+01					
SO3		8.10E+03		8.10E+03					
SOLIDS		2.27E+00		2.27E+00					
SH2									
SRO		1.24E-01		1.24E-01					
TC2O7		6.76E+00		6.76E+00					
TiO2		2.48E-05		2.48E-05					
UO3		1.25E+01		1.25E+01					
WCl		4.61E-06		4.61E-06					
ZnO		6.78E+00		6.78E+00					
ZrO2		1.59E-04		1.59E-04					

APPENDIX C ENVIRONMENTAL SIMULATION PROGRAM

Shelton (1996) provides the supernate (i.e., soluble) inventories and ionic molarities for Phase 1 feeds. Shelton's inventory is not charge balanced, however. To facilitate rigorous thermodynamic calculations, the Water Analyzer feature of ESP balances ionic charges by adding or subtracting the necessary amount of OH^- . The Stream Manager feature of ESP then converts the balanced ionic composition to the "OLI Defined Stream". The "OLI Defined Stream" contains 55.5 mol of water plus several molecular species in amounts that are equivalent to the balanced ionic composition. The "OLI Defined Stream" is compatible with the data entry format required by the ESP calculation engines, which is the input for chemical equilibrium calculations.

Exhibit 1 -- Conversion of Raw Composition Data to ESP Input

Exhibit 2 -- Typical ESP Equilibrium Results

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Exhibit 1 -- Conversion of Raw Composition Data to ESP Input

MW	CONCENTRATION ESTIMATES				ESP	
	Supernatant Chemical	105AN (M)	g/L	mg/L	mg/L	Ion
1.08E+02	Ag +	0	0	0.0		
9.50E+01	Al(OH)4-	1.74	Al+3	46.98	46980.0	Al+3
7.49E+01	As + 5	0		0	0.0	
1.08E+01	B + 3	0		0	0.0	
1.37E+02	Ba + 2	0		0	0.0	
9.01E+00	Be + 2	0		0	0.0	
2.09E+02	Bi + 3	0		0	0.0	
4.01E+01	Ca + 2	5.81E-06		0.000233	0.2	0.2 Ca+2
1.12E+02	Cd + 2	0		0	0.0	
1.40E+02	Ce + 3	0		0	0.0	
1.20E+02	Cr(OH)4-	0.013	Cr+3	0.676	676.0	676.0 Cr+3
6.35E+01	Cu + 2	0		0	0.0	
5.58E+01	Fe + 3	0.0002		0.011169	11.2	
2.01E+02	Hg + 2	0		0	0.0	
3.91E+01	K +	0.157		6.138433	6138.4	6138.4 K+
1.39E+02	La + 3	0		0	0.0	
6.94E+00	Li +	0		0	0.0	
2.43E+01	Mg + 2	0		0	0.0	
5.49E+01	Mn + 4	0		0	0.0	
9.69E+01	MnO2	0		0	0.0	
9.59E+01	Mo + 6	0		0	0.0	
2.30E+01	Na +	12		276	276000.0	276000.0 Na+
5.87E+01	Ni + 3	0		0	0.0	
2.07E+02	Pb + 4	0		0	0.0	
8.55E+01	Rb +	0		0	0.0	
1.86E+02	Re + 7	0		0	0.0	
1.03E+02	Rh + 3	0		0	0.0	
1.01E+02	Ru + 3	0		0	0.0	
1.22E+02	Sb + 5	0		0	0.0	
7.90E+01	Se + 6	0		0	0.0	
2.81E+01	Si + 4	0		0	0.0	
1.19E+02	Sn + 4	0		0	0.0	
1.50E+02	Sm + 3	0		0	0.0	
1.28E+02	Te + 6	0		0	0.0	
2.32E+02	Th + 4	0		0	0.0	
4.79E+01	Ti + 4	0		0	0.0	
2.04E+02	Tl + 3	0		0	0.0	
1.00E+00	U g/l	0.000233	UO2+2	0.000264	0.3	0.3 UO2+2
5.09E+01	V + 5	0		0	0.0	
1.84E+02	W + 6	0		0	0.0	
6.54E+01	Zn + 2	0		0	0.0	
9.12E+01	Zr + 4	0		0	0.0	
6.00E+01	CO3-2	0.363		21.78334	21783.3	21783.3 CO3-2
3.55E+01	CL	0.24		8.50872	8508.7	8508.7 Cl-
1.90E+01	F-	0.000123		0.00233	2.3	2.3 F-
9.61E+01	SO4-2	0.0682		6.551128	6551.1	6551.1 SO4-2
6.20E+01	NO3-	3.12		193.4553	193455.3	193455.3 NO3-
4.60E+01	NO2-	2.61		120.0744	120074.4	120074.4 NO2-
9.50E+01	PO4-3	0.02		1.899428	1899.4	1899.4 PO4-3
1.70E+01	OH-	3.64		61.90657	61906.6	61906.6 OH-
1.00E+00	TOC g/l	3.88	EDTA g/L	9.312	9312.0	9312.0 EDTA-4

Exhibit 2 -- Typical ESP Equilibrium Results

STREAM: an105str				
POINT : 1				
Phases----->	Aqueous	Solid	Vapor	Organic
Temperature, C	40	40	40	40
Pressure, atm	1	1	1	1
pH	15.252			
Total mol/hr	107.63	0.58632	0	0
	mol/hr-----	mol/hr-----	mol/hr-----	mol/hr-----
H2O	67.633	0	0	0
H2F2	1.22E-35	0	0	0
CO2	1.57E-17	0	0	0
H2SO4	1.22E-35	0	0	0
H4EDTA	1.22E-35	0	0	0
HCL	5.47E-31	0	0	0
HF	1.39E-17	0	0	0
HNO2	1.56E-13	0	0	0
HNO3	6.71E-19	0	0	0
SO3	1.22E-35	0	0	0
ALOH3	3.18E-10	0	0	0
CACO3	4.54E-20	0	0	0
CASO4	4.95E-16	0	0	0
ALHEDTA	1.22E-35	0	0	0
CRIIIHEDTA	9.31E-29	0	0	0
CROH3	3.64E-08	0	0	0
KCL	1.16E-04	0	0	0
KHSO4	5.33E-21	0	0	0
NAF	2.15E-05	0	0	0
NAHCO3	1.49E-07	0	0	0
NANO3	4.00E-02	0.57369	0	0
ALF3	1.22E-35	0	0	0
UO22EDTA	1.22E-35	0	0	0
UO2CL2	1.98E-30	0	0	0
UO2CO3	1.25E-21	0	0	0
UO2F2	1.42E-28	0	0	0
UO2OH2	6.19E-11	0	0	0
UO2SO4	1.09E-29	0	0	0
OHION	5.9079	0	0	0
ALF2ION	8.74E-35	0	0	0
ALF4ION	1.22E-35	0	0	0
ALF5ION	1.22E-35	0	0	0
ALF6ION	1.22E-35	0	0	0
ALFION	1.22E-35	0	0	0
ALION	1.22E-35	0	0	0
ALOH2ION	2.43E-19	0	0	0
ALOH4ION	3.0376	0	0	0
ALOHION	3.15E-30	0	0	0

Exhibit 2 -- Typical ESP Equilibrium Results

STREAM: an105str				
POINT : 1				
Phases----->	Aqueous	Solid	Vapor	Organic
Temperature, C	40	40	40	40
Pressure, atm	1	1	1	1
pH	15.252			
Total mol/hr	107.63	0.58632	0	0
	mol/hr-----	mol/hr-----	mol/hr-----	mol/hr-----
CAEDTAION	8.71E-06	0	0	0
CAFION	1.98E-16	0	0	0
CAH2PO4ION	9.28E-27	0	0	0
CAHCO3ION	1.47E-21	0	0	0
CAHEDTAION	1.29E-18	0	0	0
CAION	2.15E-12	0	0	0
CAOHION	6.48E-11	0	0	0
CAPO4ION	2.68E-10	0	0	0
CLION	0.4186	0	0	0
CO3ION	0.46304	0	0	0
CRFION	1.57E-29	0	0	0
CRIIICLION	2.21E-32	0	0	0
CRIIICL2ION	3.01E-34	0	0	0
CRIIIEDTAION	3.19E-14	0	0	0
CRIIIH2PO4ION	1.22E-35	0	0	0
CRIIIHPO4ION	5.24E-29	0	0	0
CRIIION	2.89E-34	0	0	0
CRIIINO3ION	3.05E-32	0	0	0
CROH2ION	1.08E-16	0	0	0
CROH4ION	2.27E-02	0	0	0
CROHION	9.79E-24	0	0	0
EDTAION	1.24E-03	0	0	0
FION	1.62E-04	0	0	0
H2EDTAION	1.39E-17	0	0	0
H2P2O7ION	5.15E-31	0	0	0
H2PO4ION	5.64E-15	0	0	0
H3EDTAION	1.04E-31	0	0	0
H3P2O7ION	1.22E-35	0	0	0
H5EDTAION	1.22E-35	0	0	0
H6EDTAION	1.22E-35	0	0	0
HCO3ION	1.46E-07	0	0	0
HEDTAION	2.48E-10	0	0	0
HF2ION	2.13E-21	0	0	0
HION	2.45E-16	0	0	0
HP2O7ION	3.04E-23	0	0	0
HPO4ION	2.11E-05	0	0	0
HSO4ION	8.97E-18	0	0	0
KEDTAION	2.40E-02	0	0	0

Exhibit 2 -- Typical ESP Equilibrium Results

STREAM: an105str				
POINT : 1				
Phases----->	Aqueous	Solid	Vapor	Organic
Temperature, C	40	40	40	40
Pressure, atm	1	1	1	1
pH	15.252			
Total mol/hr	107.63	0.58632	0	0
	mol/hr-----	mol/hr-----	mol/hr-----	mol/hr-----
KION	0.24907	0	0	0
KSO4ION	6.92E-04	0	0	0
NACO3ION	0.15762	0	0	0
NAEDTAION	3.11E-02	0	0	0
NAION	20.112	0	0	0
NASO4ION	5.02E-03	0	0	0
NO2ION	4.5534	0	0	0
NO3ION	4.8296	0	0	0
ALEDTAION	1.19E-25	0	0	0
P2O7ION	7.16E-15	0	0	0
PO4ION	3.49E-02	0	0	0
SO4ION	0.11324	0	0	0
UO22OH2ION	1.31E-31	0	0	0
UO23OH5ION	2.03E-23	0	0	0
UO2CLION	8.07E-28	0	0	0
UO2CO32ION	1.53E-13	0	0	0
UO2CO33ION	1.94E-06	0	0	0
UO2F3ION	1.01E-28	0	0	0
UO2F4ION	1.24E-30	0	0	0
UO2FION	7.43E-27	0	0	0
UO2HEDTAION	2.20E-29	0	0	0
UO2ION	1.12E-28	0	0	0
UO2OHION	4.06E-18	0	0	0
UO2SO42ION	1.68E-29	0	0	0
KOH	0	0	0	0
NAOH	0	0	0	0
NAPHOH	0	0	0	0
UCL6	0	0	0	0
AL2SO43	0	0	0	0
ALCL3	0	0	0	0
ALNO23	0	0	0	0
ALNO33	0	0	0	0
CAH2EDTA	0	0	0	0
CAHCO32CO3	0	0	0	0
CAHCO32	0	0	0	0
CAHCO32SO4	0	0	0	0
CAHCO3CL	0	0	0	0
CAHCO3HCO3	0	0	0	0

Exhibit 2 -- Typical ESP Equilibrium Results

STREAM: an105str				
POINT : 1				
Phases----->	Aqueous	Solid	Vapor	Organic
Temperature, C	40	40	40	40
Pressure, atm	1	1	1	1
pH	15.252			
Total mol/hr	107.63	0.58632	0	0
	mol/hr-----	mol/hr-----	mol/hr-----	mol/hr-----
CAHCO3HSO4	0	0	0	0
CAHCO3OH	0	0	0	0
CAHSO42	0	0	0	0
CAOHCL	0	0	0	0
CAOH2	0	0	0	0
CRIIIINO33	0	0	0	0
H3PO4	0	0	0	0
H4P2O7	0	0	0	0
H2CO3	0	0	0	0
KH3EDTA	0	0	0	0
NAH3EDTA	0	0	0	0
H6F6	0	0	0	0
ALOOH	0	0	0	0
KNO2	0	0	0	0
KNO3	0	0	0	0
NA2CO3	0	0	0	0
NA2SO4	0	0	0	0
NAALO2	0	0	0	0
NACL	0	0	0	0
NANO2	0	0	0	0
NA2CO3.1H2O	0	1.26E-02	0	0
NA3PO4.6H2O	0	0	0	0
NA3PO4.8H2O	0	0	0	0
NAOH.1H2O	0	0	0	0
NAPHOH.12H2O	0	0	0	0
	=====	=====	=====	=====
Total g/hr	2683.2	50.327	0	0
Volume, L/hr	1.8579	2.23E-02	0	0
Enthalpy, cal/hr	-7.71E+06	-6.82E+04	0	0
Density, g/L	1444.2	2256.7		
Vapor fraction	0	0	0	0
Solid fraction	0	1	0	0
Organic fraction	0	0	0	0
Osmotic Pres, atm	1100.6			
Ionic Strength	17.412			

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TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

APPENDIX D INVENTORY ESTIMATE FOR ENVELOPE D

Source: Phase 1 High-Level Waste Pretreatment and Staging Plan
WHC-SD-WM-ES-370 Revision 0

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Table D-1 Inventory Assumptions for 241-AZ-101 (4 sheets)

Phase	Soluble	Insoluble
Total Mass Flow (MT)	4.30E+03	1.32E+02
Volume (L)	3.44E+06	8.25E+04
Specific Gravity	1.25	1.60

Radionuclides (Ci)	Soluble	Insoluble
Am-241	8.65E+02	2.80E+04
C-14	1.88E+02	1.55E+01
Cm-244	1.91E+01	7.14E+02
Co-60	0.00E+00	0.00E+00
Cs-137	6.09E+06	2.40E+05
Ba-137	5.79E+06	2.28E+05
Eu-154	0.00E+00	0.00E+00
Np-237	0.00E+00	0.00E+00
Pu-239	1.08E+00	5.41E+02
Pu-240	0.00E+00	0.00E+00
Pu-241	0.00E+00	0.00E+00
Sr-90	2.84E+05	5.19E+06
Y-90	2.84E+05	5.19E+06
Tc-99	6.74E+02	1.47E+02
Total Curies	1.25E+07	1.09E+07

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Table D-1 Inventory Assumptions for 241-AZ-101 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
Ag+	0.00E+00	0.00E+00
Al+3	0.00E+00	1.16E+01
Am+3	2.52E-04	8.15E-03
As+5	2.65E-03	1.34E-01
B+3	8.99E-04	7.09E-02
Ba+2	9.50E-05	1.75E-01
Be+2	1.08E-06	4.21E-03
Bi+3	0.00E+00	0.00E+00
Ca+2	1.60E-03	5.85E-01
Cd+2	5.88E-05	1.36E+00
CE+3	2.42E-03	2.91E-01
Cm+3	2.36E-07	8.81E-06
Co+3	7.50E-07	8.35E-07
Cr+3	0.00E+00	1.90E-01
Cs+	2.73E-01	1.08E-02
Cu+2	2.08E-04	1.04E-01
Eu+3	0.00E+00	0.00E+00
Fe+2	0.00E+00	0.00E+00
Fe+3	4.84E-04	2.41E+01
H+	0.00E+00	0.00E+00
Hg+2	0.00E+00	0.00E+00
K+	6.82E-01	7.38E-01
La+3	1.82E-04	9.07E-01
Li+	4.50E-04	1.71E-02
Mg+2	8.64E-05	1.47E-01
Mn+2	0.00E+00	0.00E+00
Mn+4	4.43E-05	7.28E-01
Mo+6	1.37E-02	1.31E-02
Na+	3.48E+02	3.90E+00
Nb+5	0.00E+00	0.00E+00
Nd+3	0.00E+00	0.00E+00
Ni+3	1.27E-04	1.07E+00
Np+4	0.00E+00	0.00E+00
Pb+4	9.59E-04	1.27E-01

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TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table D-1 Inventory Assumptions for 241-AZ-101 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
Pd+2	0.00E+00	0.00E+00
Pu+4	1.75E-05	8.73E-03
Rb+	0.00E+00	0.00E+00
Re+7	2.25E-04	1.36E-02
Rh+3	1.61E-03	1.04E-01
Ru+3	7.68E-04	2.13E-01
Sb+5	2.08E-03	6.54E-01
Se+6	3.90E-03	4.29E-01
Si+4	5.66E-02	1.35E+00
Sm+3	0.00E+00	0.00E+00
Sn+4	0.00E+00	0.00E+00
Sr+2	9.84E-03	1.79E-01
Te+6	4.17E-03	4.61E-01
Th+4	3.37E-03	2.96E-01
Ti+4	1.20E-03	1.58E-01
Tl+3	4.17E-02	1.58E+00
UO2+2	9.24E-03	1.49E+00
V+5	1.44E-04	6.05E-03
W+6	0.00E+00	0.00E+00
Zn+2	2.14E-04	9.76E-02
Zr+4	0.00E+00	0.00E+00
Al(OH)4-	1.21E+02	0.00E+00
B02-	0.00E+00	0.00E+00
B03-2	0.00E+00	0.00E+00
C204-2	0.00E+00	0.00E+00
Cl-	6.09E-01	2.68E-02
CO3-2	1.02E+02	3.67E+00
Cr(OH)4-	4.80E-01	0.00E+00
F-	5.93E+00	1.48E-01
FeCN6-3	0.00E+00	0.00E+00
HCOO-	0.00E+00	0.00E+00
I-	3.42E-04	2.50E-04
NO2-	2.03E+02	1.69E+00
NO3-	2.36E+02	1.38E+00

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 TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table D-1 Inventory Assumptions for 241-AZ-101 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
OH-	3.31E+01	5.49E+01
P04-3	3.91E-02	5.58E-02
PTA-3	0.00E+00	0.00E+00
S04-2	2.20E-02	6.18E-03
Tc04-	6.57E-02	1.43E-02
C-14	0.00E+00	0.00E+00
Cancrinite	0.00E+00	0.00E+00
H2O	3.25E+03	0.00E+00
MnO2	0.00E+00	0.00E+00
Ni2FeCN6	0.00E+00	0.00E+00
P2O5:24WO2:44H2O	0.00E+00	0.00E+00
Organic Carbon	3.60E+00	2.02E+00
ZrO2:2H2O	1.29E-04	1.48E+01

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 TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table D-2 Inventory Assumptions for 241-AZ-102 (4 sheets)

Phase	Soluble	Insoluble
Total Mass Flow (MT)	4.03E+03	1.88E+02
Volume (L)	3.22E+06	1.18E+05
Specific Gravity	1.25	1.60

Radionuclides (Ci)	Soluble	Insoluble
Am-241	1.68E+00	1.68E+04
C-14	1.34E+02	1.24E+01
Cm-244	0.00E+00	5.41E+02
Co-60	0.00E+00	0.00E+00
Cs-137	3.18E+06	2.87E+05
Ba-137	3.02E+06	2.73E+05
Eu-154	0.00E+00	0.00E+00
Np-237	0.00E+00	0.00E+00
Pu-239	4.02E+01	4.82E+02
Pu-240	0.00E+00	0.00E+00
Pu-241	0.00E+00	0.00E+00
Sr-90	8.94E+03	2.97E+06
Y-90	8.94E+03	2.97E+06
Tc-99	3.01E+02	1.47E+02
Total Curies	6.22E+06	6.52E+06

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TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Table D-2 Inventory Assumptions for 241-AZ-102 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
Ag+	0.00E+00	0.00E+00
Al+3	0.00E+00	1.54E+01
Am+3	4.90E-07	4.90E-03
As+5	4.15E-03	1.66E-01
B+3	2.30E-03	1.39E-01
Ba+2	3.21E-04	1.59E-01
Be+2	2.12E-05	3.84E-03
Bi+3	0.00E+00	0.00E+00
Ca+2	1.12E-02	8.11E-01
Cd+2	3.61E-04	4.32E+00
CE+3	4.07E-03	2.22E-01
Cm+3	0.00E+00	6.68E-06
Co+3	3.74E-08	5.36E-08
Cr+3	0.00E+00	3.61E-01
Cs+	1.43E-01	1.29E-02
Cu+2	2.94E-04	1.00E-01
Eu+3	0.00E+00	0.00E+00
Fe+2	0.00E+00	0.00E+00
Fe+3	3.05E-03	3.77E+01
H+	0.00E+00	0.00E+00
Hg+2	0.00E+00	0.00E+00
K+	2.61E-01	3.37E-01
La+3	6.53E-04	1.29E+00
Li+	2.95E-04	8.07E-03
Mg+2	3.68E-04	2.73E-01
Mn+2	0.00E+00	0.00E+00
Mn+4	2.77E-04	8.29E-01
Mo+6	6.75E-03	6.75E-03
Na+	1.84E+02	1.19E+01
Nb+5	0.00E+00	0.00E+00
Nd+3	0.00E+00	0.00E+00
Ni+3	7.02E-04	2.55E+00
Np+4	0.00E+00	0.00E+00
Pb+4	1.44E-03	3.15E-01

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Table D-2 Inventory Assumptions for 241-AZ-102 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
Pd+2	0.00E+00	0.00E+00
Pu+4	6.49E-04	7.77E-03
Rb+	0.00E+00	0.00E+00
Re+7	2.19E-04	2.06E-02
Rh+3	2.80E-03	1.19E-01
Ru+3	6.95E-04	5.16E-02
Sb+5	0.00E+00	0.00E+00
Se+6	3.41E-03	2.93E-01
Si+4	1.80E+00	1.21E+00
Sm+3	0.00E+00	0.00E+00
Sn+4	0.00E+00	0.00E+00
Sr+2	9.15E-04	1.17E-01
Te+6	8.64E-04	9.85E-02
Th+4	0.00E+00	0.00E+00
Ti+4	2.45E-04	2.21E-02
Tl+3	5.98E-04	1.59E-02
UO2+2	5.77E+00	3.94E+00
V+5	2.57E-04	9.16E-03
W+6	0.00E+00	0.00E+00
Zn+2	1.39E-04	4.04E-02
Zr+4	0.00E+00	0.00E+00
Al(OH)4-	1.78E+01	0.00E+00
BO2-	0.00E+00	0.00E+00
BO3-2	0.00E+00	0.00E+00
C2O4-2	0.00E+00	0.00E+00
Cl-	0.00E+00	4.23E-02
CO3-2	9.42E+01	2.24E+01
Cr(OH)4-	7.65E+00	0.00E+00
F-	3.35E+00	3.57E-02
FeCN6-3	0.00E+00	0.00E+00
HCOO-	0.00E+00	0.00E+00
I-	8.56E-05	2.39E-04
NO2-	9.24E+01	1.09E+00
NO3-	7.72E+01	3.02E-01

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Table D-2 Inventory Assumptions for 241-AZ-102 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
OH-	5.41E+00	7.08E+01
PO4-3	3.30E-02	8.64E-02
PTA-3	0.00E+00	0.00E+00
S04-2	5.59E+01	3.94E-03
Tc04-	2.93E-02	1.43E-02
C-14	0.00E+00	0.00E+00
Cancrinite	0.00E+00	0.00E+00
H2O	3.48E+03	0.00E+00
MnO2	0.00E+00	0.00E+00
Ni2FeCN6	0.00E+00	0.00E+00
P2O5:24WO2:44H2O	0.00E+00	0.00E+00
Organic Carbon	4.97E+00	7.91E-01
ZrO2:2H2O	1.18E-03	9.16E+00

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Table D-3 Inventory Assumptions for 241-AY-102 (4 sheets)

Phase	Soluble	Insoluble
Total Mass Flow (MT)	3.18E+03	7.55E+01
Volume (L)	2.54E+06	4.72E+04
Specific Gravity	1.25	1.60

Radionuclides (Ci)	Soluble	Insoluble
Am-241	3.61E-01	3.26E+03
C-14	0.00E+00	1.81E-01
Cm-244	1.42E-02	0.00E+00
Co-60	0.00E+00	0.00E+00
Cs-137	5.40E+03	1.92E+04
Ba-137	5.13E+03	1.83E+04
Eu-154	0.00E+00	0.00E+00
Np-237	0.00E+00	0.00E+00
Pu-239	4.61E-01	6.59E+02
Pu-240	0.00E+00	0.00E+00
Pu-241	0.00E+00	0.00E+00
Sr-90	3.69E+03	1.97E+06
Y-90	3.69E+03	1.97E+06
Tc-99	2.47E+01	0.00E+00
Total Curies	1.79E+04	3.99E+06

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Table D-3 Inventory Assumptions for 241-AY-102 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
Ag+	2.82E-02	1.04E+00
Al+3	0.00E+00	5.49E+00
Am+3	1.05E-07	9.50E-04
As+5	0.00E+00	0.00E+00
B+3	0.00E+00	0.00E+00
Ba+2	2.06E-03	2.89E-01
Be+2	0.00E+00	0.00E+00
Bi+3	0.00E+00	0.00E+00
Ca+2	1.25E-02	2.04E+00
Cd+2	3.89E-04	6.03E-02
CE+3	0.00E+00	0.00E+00
Cm+3	1.75E-10	0.00E+00
Co+3	0.00E+00	0.00E+00
Cr+3	0.00E+00	4.87E-01
Cs+	3.35E-04	1.20E-03
Cu+2	0.00E+00	0.00E+00
Eu+3	0.00E+00	0.00E+00
Fe+2	0.00E+00	0.00E+00
Fe+3	1.22E-03	1.22E+01
H+	0.00E+00	0.00E+00
Hg+2	0.00E+00	0.00E+00
K+	1.81E-01	1.47E-01
La+3	1.73E-04	5.75E-01
Li+	0.00E+00	0.00E+00
Mg+2	0.00E+00	0.00E+00
Mn+2	0.00E+00	0.00E+00
Mn+4	0.00E+00	1.28E+00
Mo+6	0.00E+00	0.00E+00
Na+	9.50E+00	2.79E+00
Nb+5	0.00E+00	0.00E+00
Nd+3	0.00E+00	0.00E+00
Ni+3	3.96E-04	4.39E-01
Np+4	0.00E+00	0.00E+00
Pb+4	0.00E+00	0.00E+00

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Table D-3 Inventory Assumptions for 241-AY-102 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
Pd+2	0.00E+00	0.00E+00
Pu+4	7.44E-06	1.06E-02
Rb+	0.00E+00	0.00E+00
Re+7	0.00E+00	0.00E+00
Rh+3	0.00E+00	0.00E+00
Ru+3	0.00E+00	0.00E+00
Sb+5	0.00E+00	0.00E+00
Se+6	0.00E+00	0.00E+00
Si+4	1.85E+00	3.96E+00
Sm+3	0.00E+00	0.00E+00
Sn+4	0.00E+00	0.00E+00
Sr+2	6.12E-04	1.20E-01
Te+6	0.00E+00	0.00E+00
Th+4	0.00E+00	0.00E+00
Ti+4	0.00E+00	0.00E+00
Tl+3	0.00E+00	0.00E+00
UO2+2	1.81E+00	8.90E-01
V+5	0.00E+00	0.00E+00
W+6	0.00E+00	0.00E+00
Zn+2	0.00E+00	0.00E+00
Zr+4	0.00E+00	0.00E+00
Al(OH)4-	2.32E-02	0.00E+00
BO2-	0.00E+00	0.00E+00
BO3-2	0.00E+00	0.00E+00
C2O4-2	0.00E+00	0.00E+00
Cl-	2.75E+00	1.56E-01
CO3-2	0.00E+00	0.00E+00
Cr(OH)4-	1.51E-01	0.00E+00
F-	6.58E-01	1.87E-01
FeCN6-3	0.00E+00	0.00E+00
HCOO-	0.00E+00	0.00E+00
I-	0.00E+00	0.00E+00
NO2-	3.46E+00	3.49E-02
NO3-	7.52E-01	2.69E-02

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Table D-3 Inventory Assumptions for 241-AY-102 (4 sheets)

Chemicals (MT)	Soluble	Insoluble
OH-	7.48E+00	3.77E+01
P04-3	3.85E-01	3.90E-03
PTA-3	0.00E+00	0.00E+00
S04-2	3.87E-01	2.00E-02
Tc04-	2.40E-03	0.00E+00
C-14	0.00E+00	0.00E+00
Cancrinite	0.00E+00	0.00E+00
H2O	3.15E+03	0.00E+00
MnO2	0.00E+00	0.00E+00
Ni2FeCN6	0.00E+00	0.00E+00
P2O5:24W02:44H2O	0.00E+00	0.00E+00
Organic Carbon	1.18E+00	5.64E+00
ZrO2:2H2O	5.20E-04	5.25E-06

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Table D-4 Inventory Assumptions for 241-C-106 (4 sheets)

Phase	Soluble	Insoluble
Total Mass Flow (MT)	9.23E+02	3.05E+02
Volume (L)	7.38E+05	1.91E+05
Specific Gravity	1.25	1.60

Radionuclides (Ci)	Soluble	Insoluble
Am-241	1.60E+01	1.11E+03
C-14	0.00E+00	2.94E-01
Cm-244	0.00E+00	0.00E+00
Co-60	4.81E+00	1.48E+02
Cs-137	6.68E+04	2.88E+05
Ba-137	6.35E+04	2.74E+05
Eu-154	0.00E+00	0.00E+00
Np-237	0.00E+00	0.00E+00
Pu-239	1.61E+02	3.22E+03
Pu-240	0.00E+00	0.00E+00
Pu-241	0.00E+00	0.00E+00
Sr-90	2.12E+02	2.12E+06
Y-90	2.12E+02	2.12E+06
Tc-99	4.01E+01	2.09E+02
Total Curies	1.31E+05	4.81E+06

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Table D-4 Inventory Assumptions for 241-C-106 (4 sheets)

Chemicals (MT)		
Ag+	1.47E-03	5.63E-01
Al+3	0.00E+00	4.36E+01
Am+3	4.66E-06	3.23E-04
As+5	0.00E+00	0.00E+00
B+3	5.41E-03	1.67E-02
Ba+2	3.13E-03	5.21E+00
Be+2	0.00E+00	0.00E+00
Bi+3	1.64E-02	5.32E-01
Cat2	4.83E-02	1.27E+01
Cd+2	1.29E-02	3.85E-01
CE+3	0.00E+00	0.00E+00
Cm+3	0.00E+00	0.00E+00
Co+3	4.26E-09	5.13E-03
Cr+3	0.00E+00	1.04E+00
Cs+	4.06E-03	1.75E-02
Cu+2	1.63E-03	1.36E-01
Eu+3	0.00E+00	0.00E+00
Fe+2	0.00E+00	0.00E+00
Fe+3	0.00E+00	5.56E+01
H+	0.00E+00	0.00E+00
Hg+2	0.00E+00	0.00E+00
K+	1.72E-01	1.46E+00
La+3	0.00E+00	0.00E+00
Li+	0.00E+00	0.00E+00
Mg+2	1.19E-02	6.98E+00
Mn+2	0.00E+00	0.00E+00
Mn+4	5.37E-03	1.99E+00
Mo+6	0.00E+00	0.00E+00
Na+	5.34E+01	8.41E+01
Nb+5	0.00E+00	0.00E+00
Nd+3	0.00E+00	0.00E+00
Ni+3	3.47E-02	1.01E+00
Np+4	0.00E+00	0.00E+00
Pb+4	4.81E-02	2.52E+00

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Table D-4 Inventory Assumptions for 241-C-106 (4 sheets)

Chemicals (MT)		
Pd+2	0.00E+00	1.70E-01
Pu+4	2.60E-03	5.19E-02
Rb+	0.00E+00	0.00E+00
Re+7	0.00E+00	0.00E+00
Rh+3	0.00E+00	0.00E+00
Ru+3	0.00E+00	0.00E+00
Sb+5	0.00E+00	0.00E+00
Se+6	0.00E+00	0.00E+00
Si+4	2.27E-02	7.57E+01
Sm+3	0.00E+00	0.00E+00
Sn+4	0.00E+00	0.00E+00
Sr+2	1.25E-05	1.25E-01
Te+6	0.00E+00	0.00E+00
Th+4	0.00E+00	0.00E+00
Ti+4	0.00E+00	0.00E+00
Tl+3	0.00E+00	0.00E+00
UO2+2	1.43E-02	6.25E-01
V+5	0.00E+00	0.00E+00
W+6	0.00E+00	0.00E+00
Zn+2	0.00E+00	4.93E-02
Zr+4	1.23E-01	2.23E+00
Al(OH)4-	7.68E-02	0.00E+00
BO2-	0.00E+00	0.00E+00
BO3-2	0.00E+00	0.00E+00
C2O4-2	0.00E+00	0.00E+00
Cl-	0.00E+00	0.00E+00
CO3-2	0.00E+00	0.00E+00
Cr(OH)4-	3.40E-03	0.00E+00
F-	0.00E+00	0.00E+00
FeCN6-3	0.00E+00	0.00E+00
HCOO-	0.00E+00	0.00E+00
I-	0.00E+00	0.00E+00
NO2-	0.00E+00	0.00E+00
NO3-	9.85E-01	4.95E-04

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Table D-4 Inventory Assumptions for 241-C-106 (4 sheets)

Chemicals (MT)		
OH-	0.00E+00	0.00E+00
P04-3	1.43E+00	8.02E+00
PTA-3	0.00E+00	0.00E+00
S04-2	5.91E+00	1.21E-01
Tc04-	3.90E-03	2.04E-02
C-14	0.00E+00	0.00E+00
Cancrinite	0.00E+00	0.00E+00
H2O	8.55E+02	0.00E+00
MnO2	0.00E+00	0.00E+00
Ni2FeCN6	0.00E+00	0.00E+00
P205:24W02:44H2O	0.00E+00	0.00E+00
Organic Carbon	5.25E+00	5.26E-03
ZrO2:2H2O	0.00E+00	0.00E+00

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Table D-5 Total Phase I HLW Tank Inventory (4 sheets)

Phase	Soluble	Insoluble
Total Mass Flow (MT)	1.24E+04	7.00E+02
Volume (L)	9.92E+06	4.38E+05
Specific Gravity	1.25	1.60

Radionuclides (Ci)	Soluble	Insoluble
Am-241	8.83E+02	4.91E+04
C-14	3.22E+02	2.84E+01
Cm-244	1.91E+01	1.26E+03
Co-60	4.81E+00	1.48E+02
Cs-137	9.34E+06	8.35E+05
Ba-137	8.88E+06	7.93E+05
Eu-154	0.00E+00	0.00E+00
Np-237	0.00E+00	0.00E+00
Pu-239	2.03E+02	4.90E+03
Pu-240	0.00E+00	0.00E+00
Pu-241	0.00E+00	0.00E+00
Sr-90	2.97E+05	1.23E+07
Y-90	2.97E+05	1.23E+07
Tc-99	1.04E+03	5.04E+02
Total Curies	1.88E+07	2.62E+07

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Table D-5 Total Phase I HLW Tank Inventory (4 sheets)

Chemicals (MT)		
Ag+	2.97E-02	1.61E+00
Al+3	0.00E+00	7.61E+01
Am+3	2.58E-04	1.43E-02
As+5	6.80E-03	3.00E-01
B+3	8.60E-03	2.27E-01
Ba+2	5.61E-03	5.83E+00
Be+2	2.23E-05	8.04E-03
Bi+3	1.64E-02	5.32E-01
Ca+2	7.37E-02	1.61E+01
Cd+2	1.37E-02	6.12E+00
CE+3	6.49E-03	5.13E-01
Cm+3	2.36E-07	1.55E-05
Co+3	7.92E-07	5.13E-03
Cr+3	0.00E+00	2.08E+00
Cs+	4.21E-01	4.24E-02
Cu+2	2.13E-03	3.40E-01
Eu+3	0.00E+00	0.00E+00
Fe+2	0.00E+00	0.00E+00
Fe+3	4.75E-03	1.30E+02
H+	0.00E+00	0.00E+00
Hg+2	0.00E+00	0.00E+00
K+	1.29E+00	2.68E+00
La+3	1.01E-03	2.77E+00
Li+	7.45E-04	2.52E-02
Mg+2	1.24E-02	7.40E+00
Mn+2	0.00E+00	0.00E+00
Mn+4	5.70E-03	4.82E+00
Mo+6	2.05E-02	1.99E-02
Na+	5.95E+02	1.03E+02
Nb+5	0.00E+00	0.00E+00
Nd+3	0.00E+00	0.00E+00
Ni+3	3.59E-02	5.07E+00
Np+4	0.00E+00	0.00E+00
Pb+4	5.05E-02	2.96E+00

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Table D-5 Total Phase I HLW Tank Inventory (4 sheets)

Chemicals (MT)		
Pd+2	0.00E+00	1.70E-01
Pu+4	3.27E-03	7.90E-02
Rb+	0.00E+00	0.00E+00
Re+7	4.43E-04	3.41E-02
Rh+3	4.41E-03	2.23E-01
Ru+3	1.46E-03	2.65E-01
Sb+5	2.08E-03	6.54E-01
Se+6	7.31E-03	7.22E-01
Si+4	3.72E+00	8.22E+01
Sm+3	0.00E+00	0.00E+00
Sn+4	0.00E+00	0.00E+00
Sr+2	1.14E-02	5.41E-01
Te+6	5.04E-03	5.60E-01
Th+4	3.37E-03	2.96E-01
Ti+4	1.45E-03	1.80E-01
Tl+3	4.23E-02	1.60E+00
UO2+2	7.61E+00	6.94E+00
V+5	4.01E-04	1.52E-02
W+6	0.00E+00	0.00E+00
Zn+2	3.53E-04	1.87E-01
Zr+4	1.23E-01	2.23E+00
Al(OH)4-	1.39E+02	0.00E+00
BO2-	0.00E+00	0.00E+00
BO3-2	0.00E+00	0.00E+00
C2O4-2	0.00E+00	0.00E+00
Cl-	3.36E+00	2.26E-01
CO3-2	1.96E+02	2.60E+01
Cr(OH)4-	8.28E+00	0.00E+00
F-	9.94E+00	3.70E-01
FeCN6-3	0.00E+00	0.00E+00
HCOO-	0.00E+00	0.00E+00
I-	4.28E-04	4.89E-04
NO2-	2.99E+02	2.82E+00
NO3-	3.15E+02	1.71E+00

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Table D-5 Total Phase I HLW Tank Inventory (4 sheets)

Chemicals (MT)		
OH-	4.60E+01	1.63E+02
P04-3	1.88E+00	8.16E+00
PTA-3	0.00E+00	0.00E+00
S04-2	6.22E+01	1.51E-01
Tc04-	1.01E-01	4.91E-02
C-14	0.00E+00	0.00E+00
Cancrinite	0.00E+00	0.00E+00
H2O	1.07E+04	0.00E+00
MnO2	0.00E+00	0.00E+00
Ni2FeCN6	0.00E+00	0.00E+00
P2O5:24W02:44H2O	0.00E+00	0.00E+00
Organic Carbon	1.50E+01	8.46E+00
ZrO2:2H2O	1.83E-03	2.39E+01

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APPENDIX E PHASE 2 MASS BALANCE WITH REVISED TWRS INVENTORY

Table E-1 Comparison of Revised TWRS Inventory and TWRS Inventory

	Metric Tons			Metric Tons	
	Revised TWRS	TWRS		Revised TWRS	TWRS
Al	7845	4530	ILAW	381000	457000
Cr	790	353	IHLW	81700	37000
Fe	1230	793			
PO4	5960	4970			
SO4	4770	2045			
Na	54200	68800			

Figure E-1 Major Components of Inventory

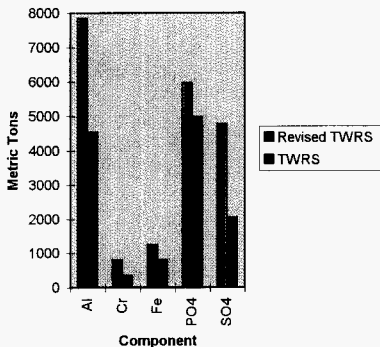
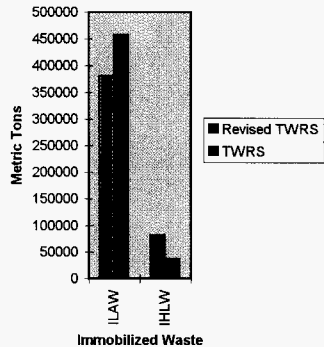


Figure E-2 Comparison of Products

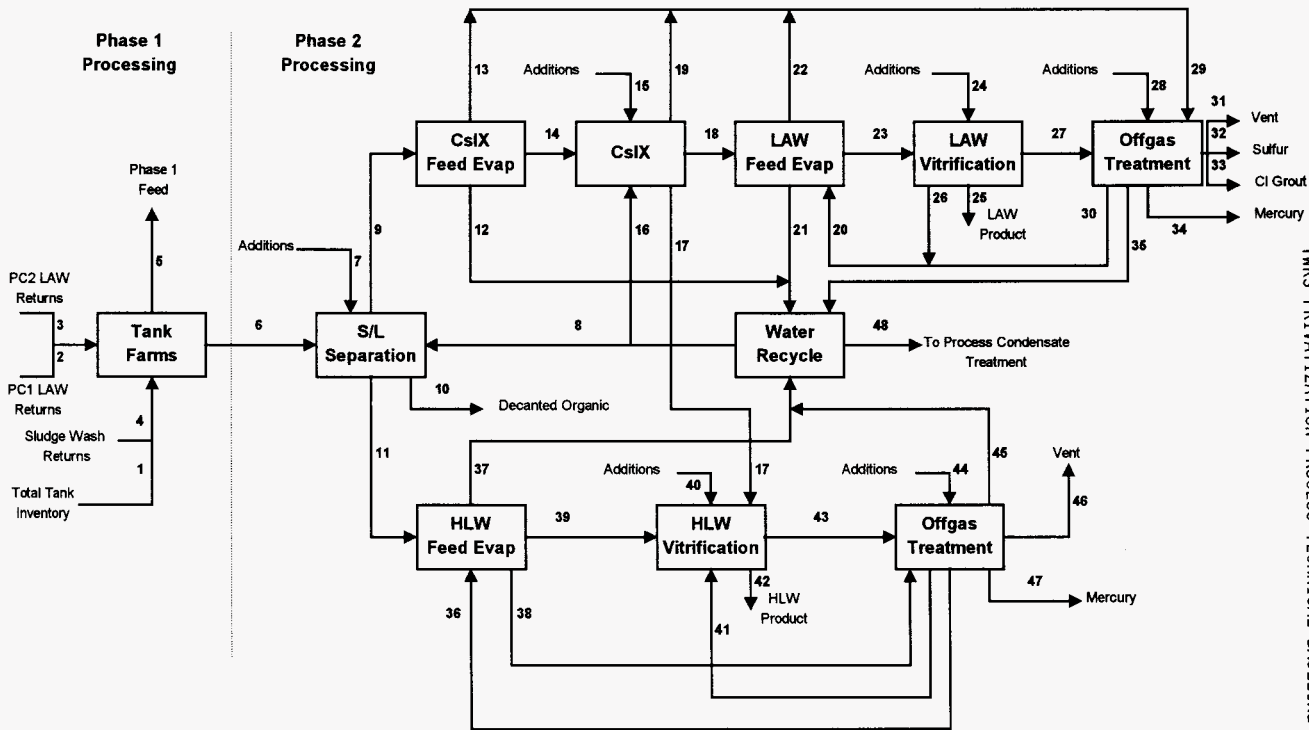


As a special case of Phase 2, several major components of the TWRS Inventory were revised with expected values from the tentative standard inventory. The table and figures above show the TWRS Inventory and the Revised TWRS Inventory total for Al, Cr, Fe, phosphate, sulfate and Na. These components were distributed to the liquid and solid phase with the same solubility factors as used in Section 3.0.

The balance of this APPENDIX presents the mass balance resulting from running the Phase 2 process model with this Revised TWRS Inventory.

The results of this APPENDIX should be regarded as an indicator of future trends because finalization of the standard inventory is not expected until late FY-1997.

Figure E-3 Phase 2 Waste Processing



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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Total Mass Flow (MT)	7.13E+05	3.75E+03	3.77E+03	9.46E+03	9.57E+04	6.34E+05	4.57E+04	5.77E+05	1.06E+06	7.78E+01
Volume (L)	5.77E+08	3.65E+06	3.71E+06	9.28E+06	7.34E+07	5.20E+08	3.04E+07	5.77E+08	9.19E+08	7.78E+04
Specific Gravity	1.24E+00	1.01E+00	1.02E+00	1.02E+00	1.30E+00	1.22E+00	1.50E+00	1.00E+00	1.16E+00	1.00E+00

Radionuclides (Ci)										
Am-241	8.00E+03	6.11E+00	5.96E+00	1.15E+02	3.35E+03	4.77E+03		5.73E-04	4.76E+03	
C-14	3.22E+03	2.09E-01	1.89E-01	3.72E+01	3.78E+02	2.88E+03		3.46E-04	2.87E+03	
Ce-137	3.18E+07	5.96E+04	3.99E+04	1.16E+06	2.70E+07	6.07E+06		6.76E-01	1.39E+07	
Ba-137	3.02E+07	5.67E+04	3.79E+04	1.10E+06	2.57E+07	5.77E+06		6.42E-01	1.32E+07	
Np-237	6.94E+00	1.60E-03	7.43E-04		3.84E-01	6.58E+00		2.17E-04	6.56E+00	
Ru-239	1.65E+03	1.16E+00	1.03E+00	1.45E+02	6.32E+02	1.16E+03		1.40E-04	1.16E+03	
Ru-240	4.30E+02	2.90E-01	2.61E-01		1.10E+02	3.20E+02		3.84E-05	3.19E+02	
Ru-241	4.76E+03	1.81E+00	1.62E+00		6.90E+02	4.08E+03		4.93E-04	4.07E+03	
Sr-90	1.88E+06	2.02E+03	2.39E+03	3.84E+04	1.21E+06	7.12E+05		8.53E-02	7.10E+05	
Y-90	1.88E+06	2.02E+03	2.39E+03	3.84E+04	1.21E+06	7.12E+05		8.53E-02	7.10E+05	
Tc-99	2.27E+04	1.73E+01	5.78E+02	1.71E+02	7.04E+03	1.64E+04		4.18E-03	1.64E+04	
Total Curies	6.58E+07	1.28E+05	8.31E+04	2.34E+06	5.51E+07	1.33E+07		1.49E+00	2.83E+07	

Chemicals (MT)										
Ag+	3.20E-01	2.22E-06	1.85E-06	2.57E-02	2.91E-02	3.16E-01		3.80E-08	3.15E-01	
Am3+	2.33E-03	1.78E-06	1.74E-06	3.36E-05	9.74E-04	1.39E-03		1.67E-10	1.39E-03	
As5+	4.05E-05				4.05E-05					
BH3	3.43E-02	3.01E-05	3.98E-05	5.05E-03	2.20E-02	1.74E-02		2.09E-09	1.73E-02	
Be+2	7.91E-01	1.01E-05	2.19E-05	4.54E-03	1.19E-02	7.84E-01		9.42E-08	7.82E-01	
Be+2	2.43E-05				2.43E-05					
Bi+3	3.01E+00	2.21E-06	1.46E-06	1.43E-02	1.64E-02	3.01E+00		4.55E-07	3.76E+00	
Ca+2	1.52E+01	9.85E-03	1.04E-02	5.41E-02	4.30E+00	1.10E+01		1.00E-04	1.35E+01	
Ca+2	7.63E+00	1.43E-04	1.48E-04	1.15E-02	7.12E-02	7.57E+00		1.21E-06	7.53E+00	
Ce+3	2.36E+00				6.17E-03	2.36E+00		2.83E-07	2.35E+00	
Co+3	5.93E-08				2.26E-07					
Co+3	1.46E-03				9.59E-08	7.47E-07		1.46E-03		
Cs+	2.14E+00	6.89E-04	4.61E-04	5.29E-02	6.10E-01	1.58E+00		8.80E-08	1.84E+00	
Cr+2	9.95E-02	1.06E-04	1.06E-04	1.47E-03	4.48E-02	5.57E-02		6.70E-09	5.56E-02	
Fu+3	1.50E+01	1.32E-02	1.48E-03	5.51E-05	5.51E+00	9.50E+00		1.41E-06	1.17E+01	
H+										
Hg+2	5.84E-02	1.42E-04	1.42E-04		5.72E-02	1.49E-03		1.79E-10	1.48E-03	
K+	7.07E+02	8.17E-01	8.00E-01	4.17E-01	3.21E+02	3.88E+02		4.69E-05	3.87E+02	
La+3	2.39E-01	8.99E-05	2.13E-04	2.31E-04	6.40E-02	1.73E-01		2.11E-08	1.73E-01	
Mg+2	1.46E-04				1.46E-04					
Mn+2	4.82E-05				4.82E-05			5.82E-12	4.84E-05	
Mn+4	1.08E+01	5.03E-03	5.10E-03	4.68E-03	2.10E+00	8.73E+00		1.02E-06	8.70E+00	
Mn+6	7.23E-03				7.23E-03			9.04E-13	5.91E-13	
Nat	5.21E+04	2.50E+01	3.48E+01	1.31E+02	1.06E+04	4.16E+04	1.25E+04		2.53E-02	5.44E+04
Ni+3	8.21E+00	7.07E-03	7.24E-03	3.03E-02	3.03E+00	5.22E+00		6.27E-07	5.21E+00	
Np+4	9.85E-03	2.27E-06	1.05E-06		5.45E-04	9.33E-03		3.07E-07	9.31E-03	
Ni+4	9.59E+00	6.32E-03	6.32E-03	4.18E-02	2.61E+00	7.02E+00		1.14E-06	7.03E+00	
Ru+4	2.86E-02	2.00E-05	1.78E-05	2.33E-03	1.07E-02	2.02E-02		2.43E-09	2.02E-02	
Rb+	2.40E-04				2.40E-04			2.89E-11	2.40E-04	
Ru+7	1.06E-04				4.21E-04					
Ru+3	8.50E-04				4.19E-03					
Ru+3	1.18E-03				1.39E-03					
Se+6	1.35E-04				1.35E-04					
Si+4	7.06E+03	8.64E-03	5.08E-03	1.84E+00	1.94E+00	6.65E+01		1.45E-09	9.45E-10	
Si+2	3.81E-01	1.43E-05	1.61E-05	1.74E-03	1.74E-02	3.65E-01		6.23E-05	1.36E+02	
Te+6	8.27E-04				4.80E-03			4.38E-08	3.64E-01	
UO2+2	4.13E+01	2.12E-02	1.08E-02	2.28E+00	1.26E+01	3.10E+01		7.58E-06	6.25E+01	
Zn+2	7.78E-04				7.78E-04					
Al(OH)4-	1.13E+04	8.99E+00	8.90E+00	1.64E+01	3.72E+03	7.82E+03		2.09E-03	1.72E+04	
BO2-								2.48E-05	1.61E-05	
Cl-	6.78E+02	4.99E-01	5.05E-01	2.43E+00	2.03E+02	4.79E+02		4.27E-04	4.77E+02	
CO3-2	3.10E+03	3.87E+00	3.63E+00	2.33E+01	1.93E+03	1.44E+03		6.23E-05	1.44E+03	
Cr(OH)4-	1.10E+03	1.03E-01	7.60E-02	1.12E+00	4.14E+01	1.05E+03		1.26E-04	1.13E+03	
F-	1.14E+03	2.46E-01	2.38E-01	1.67E+00	1.05E+02	1.04E+03		2.68E-04	1.03E+03	
I-	9.07E-02				5.05E-05	4.06E-04		7.04E-07	8.96E-02	
NO2-	9.80E+03	9.33E+00	8.99E+00	4.04E+01	3.33E+03	5.59E+03	2.79E+02		5.76E+03	
NO3-	1.07E+05	1.88E+01	1.90E+01	3.85E+01	7.94E+03	9.94E+04		2.93E-02	9.91E+04	
OH-	6.40E+03	4.21E+00	1.15E+01	1.99E+01	1.72E+03	4.72E+03	9.14E+03		1.34E-03	1.24E+04
PO4-3	5.43E+03	3.17E-01	3.22E-01	1.58E+00	1.32E+02	5.32E+03		8.03E-04	5.27E+03	
SO4-2	4.67E+03	1.04E+00	8.41E-01	1.23E+01	4.20E+02	4.27E+03		5.14E-04	4.25E+03	
TO4-	2.21E+00	1.70E-03	5.63E-02	1.67E-02	6.85E-01	1.60E+00		4.07E-07	1.59E+00	
H2O	5.08E+05	3.67E+03	3.68E+03	9.16E+03	6.41E+04	4.61E+05	2.36E+04		5.77E+05	
Separable Organic Organic Carbon	8.80E+01	1.06E+03	1.78E+00	6.59E+00	7.34E+02	3.37E+02		7.80E+00	3.36E+02	7.78E+01
ZnO2+2H2O	7.53E+00			6.08E-04	1.74E-03	7.53E+00		9.04E-07	7.51E+00	

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
LIQUID COMPONENTS										
Chemicals Continued (MT)										
H ₂								1.03E-08	6.70E-09	
SO ₂								4.97E-12	3.24E-12	
Cl ₂										
CO										
CO ₂										
F ₂										
H ₂										
I ₂										
N ₂										
N ₂ O										
NO										
NO ₂										
O ₂										
SO ₂										
Glycolic Anion								2.23E-07	1.46E-07	
H ₂ S										
Glycolic Acid										
Kerosene										
NE ₃										
Polyelectrolyte							1.90E+02	2.85E-06	2.08E+01	
Sulfur										

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Total Mass Flow (MT)	2.87E+04		4.33E-03	5.04E+00	5.53E+02	2.81E+04				2.38E+02
Radionuclides (Ci)										
Am-241	9.75E+04		7.38E+02	2.88E+02	3.76E+04	6.11E+04			8.03E+02	
C-14	2.12E+03			1.64E-01	2.11E+01	2.10E+03			2.73E+01	
Cs-137	1.39E+07			6.01E+03	6.81E+05	1.32E+07			7.01E+04	
Ba-137	1.32E+07			5.71E+03	6.47E+05	1.26E+07			6.66E+04	
Np-237	6.27E-01					6.27E+01			8.25E-01	
Pu-239	2.53E+04		3.35E+01	3.99E+01	4.19E+03	2.12E+04			2.78E+02	
Pu-240	6.26E+03		8.38E+00			6.28E+03			8.23E+01	
Pu-241	6.93E+04					6.93E+04			9.14E+02	
Sr-90	5.18E+07			3.42E+05	7.72E+04	9.39E+06			5.62E+05	
Y-90	5.18E+07			3.42E+05	7.72E+04	9.39E+06			5.62E+05	
Tc-99	9.32E+03			3.79E+00	4.29E+02	8.87E+03			1.17E+02	
Total Curies	1.31E+08		6.85E+05		1.67E+05	2.02E+07			1.26E+06	
Chemicals (MT)										
Ag+	1.48E+00			9.25E-03	9.33E-01	5.56E-01			7.31E-03	
Al+3	4.59E+03			6.07E-01	6.50E+01	4.53E+03			2.40E+01	
Am+3	2.84E-02		2.15E-04	8.38E-05	1.10E-02	1.78E-02			2.34E-04	
As+5	2.26E-03				2.25E-03					
Be+2	3.74E+00				3.74E+00					
Be+2	3.08E-03				3.08E-03					
Bi+3	2.60E+02			5.20E-03	5.27E-01	2.59E+02			3.40E+00	
Bi+3	1.46E+02			1.40E-01	1.43E+01	1.32E+02			1.70E+00	
Cl-2	6.53E+00			3.76E-02	4.23E+00	2.37E+00			3.11E-02	
Co+3	2.35E+02			3.04E-03	3.95E-01	2.35E+02			3.09E+00	
Cu+3	1.76E-05			9.16E-08	1.20E-05	5.71E-06			7.51E-08	
Co+3	1.49E-06			5.02E-05	5.17E-05					
Cu+3	3.18E+02			1.52E-02	1.60E+00	3.13E+02			3.70E+00	
Cs+	4.73E-01			3.16E-04	3.53E-02	4.38E-01			2.32E-03	
Cr+2	1.86E-01			1.88E-01	1.88E-01					
Fe+3	1.22E+03			9.50E-01	1.04E+02	1.12E+03			1.46E+01	
Hg+2	8.81E-02					8.81E-02			1.16E-03	
K+	2.96E+01			2.11E-02	2.37E+00	2.72E+01			3.58E-01	
La+3	2.30E+01			1.51E-02	1.80E+00	2.13E+01			2.79E-01	
Mg+2	6.22E+00			7.07E-02	7.21E+00	1.12E+00			1.47E-02	
Mn+4	1.80E+02			3.32E-02	3.99E+00	1.76E+02			2.32E+00	
Mb+6	3.21E-02			1.18E-04	1.58E-02	1.63E-02			2.13E-04	
Nat	2.38E+03			9.25E-01	9.50E+01	2.29E+03			1.66E+01	
Ni+3	2.06E+02			3.28E-02	3.65E+00	2.02E+02			2.66E+00	
Np+4	8.90E-02					8.90E-02			1.17E-03	
Pb+4	2.93E+01			2.73E-02	2.82E+00	2.65E+01			3.49E-01	
Pu+4	4.36E-01			6.43E-04	6.77E-02	3.70E-01			4.86E-03	
Ru+3	1.93E-01		5.77E-04	1.32E-03	1.65E-01	2.96E-02			3.90E-04	
Se+6	3.31E+00			4.27E-03	5.61E-01	2.76E+00			3.62E-02	
Si+4	6.22E+02			7.66E-01	7.84E+01	5.44E+02			6.23E+00	
Sn+2	3.66E+01		2.43E-03	3.40E-03	3.99E-01	3.62E+01			4.75E-01	
Ti+4	2.79E+00			1.75E-03	2.66E-01	2.52E+00			3.32E-02	
Tl+4	1.55E-01				1.55E-01					
UO ₂	1.61E+03			4.15E-02	4.65E+00	1.61E+03			2.07E+01	
Zn+2	5.06E-01			1.30E-03	1.61E-01	3.47E-01			4.53E-03	
C2	8.99E+00			9.68E-04	1.05E-01	8.90E+00			1.17E-01	
CO ₂	1.09E+02			1.55E-01	1.68E+01	9.25E+01			1.22E+00	
F-	6.82E+01			1.75E-03	2.21E-01	6.80E+01			8.94E-01	
I-	1.40E-03			2.69E-06	3.68E-04	1.04E-03			1.36E-05	
NO ₂	4.63E+01			1.64E-02	2.19E+00	5.96E+01			7.84E-01	
NO ₃	9.85E+02			1.01E-02	1.43E+00	9.85E+02			1.30E+01	
OH-	1.36E+04		1.13E-03	8.81E-01	1.05E+02	1.34E+04			9.90E+01	
RO ₄ -3	5.94E+02			7.71E-02	8.04E+00	5.86E+02			2.33E+00	
SO ₄ -2	1.03E+02			1.31E-03	1.34E-01	1.03E+02			1.37E+00	
TCO ₄ -1	9.07E-01			3.69E-04	4.17E-02	8.64E-01			1.14E-02	
H ₂ O										
M ₂ O ₃										
Organic Carbon	8.73E+01			3.67E-02	4.32E+00	8.30E+01			1.09E+00	
ZrO ₂ .2H ₂ O	1.20E+03			1.42E-01	1.86E+01	1.18E+03			1.56E+01	
As ₂ O ₃										
Al ₂ O ₃										
Am ₂ O ₃										
B ₂ O ₃										
B ₂ O										
B ₁₂ O ₃										
CaO										

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	1	2	3	4	5	6	7	8	9	10
SOLID COMPONENTS										
Chemicals Continued (MT)										
CaO										
Ca2O3										
Ca2O3										
Ca2O3										
Ca2O										
Cl2										
F2O3										
H2										
H2O										
K2O										
La2O3										
Li2O										
MgO										
MnO										
Mn2O3										
Na2O										
Ni2O3										
BiO2										
R2O2										
Rb2O										
Rh2O3										
SeO3										
SiO2										
SO3										
SnO										
Ta2O7										
TiO2										
UO3										
ZnO										
ZrO2										
Cement										
Flyash										
Polyelectrolyte										
CS-100 - Na Form									1.64E+00	

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Total Mass Flow (MT)	2.02E+05	5.73E+05	6.39E+03	4.80E+05	7.24E+04	1.36E+04	8.84E+03	5.56E+05	9.33E+02	6.80E+05
Volume (L)	2.04E+08	5.73E+08	6.39E+06	3.38E+08	7.10E+07	1.36E+07	7.94E+06	4.14E+08	9.28E+05	6.69E+08
Specific Gravity	1.01E+00	1.02E+00	1.02E+00	1.42E+00	1.02E+00	1.00E+00	1.11E+00	1.34E+00	1.01E+00	1.02E+00
Radionuclides (Ci)										
Am-241	1.23E+01	5.76E-04	5.77E-07	4.76E+03		1.36E-05		4.76E+03		
C-14	7.40E+00	3.47E-04	3.48E-07	2.87E+03		8.18E-06		2.87E+03		
Ce-137	1.31E+05	1.68E+00	1.63E-03	1.39E+07		1.60E-02		4.86E+05	1.03E-02	2.90E+05
Be-137	1.28E+05	1.59E+00	1.60E-03	1.36E+07		1.52E-02	1.34E+07	4.63E+05	9.75E-03	2.75E+05
Np-237	1.70E-02	7.94E-07	7.95E-10	6.56E+00		5.12E-06	1.27E+07	6.56E+00		2.58E+03
Pu-239	2.99E+00	1.40E-04	1.40E-07	1.16E+03		3.30E-06		1.16E+03		
Pu-240	8.22E-01	3.84E-05	3.83E-08	3.19E+02		9.09E-07		3.19E+02		
Pu-241	0.05E+01	4.82E-04	4.83E-07	4.07E+03		1.16E-05		4.07E+03		
Sr-90	1.83E+03	8.59E-02	8.60E-05	7.10E+05		2.02E-03		7.10E+05		
Y-90	1.83E+03	8.59E-02	8.60E-05	7.10E+05		2.02E-03		7.10E+05		
Tl-99	4.22E+01	1.93E-03	1.93E-06	1.64E+04		9.89E-05		1.64E+04		
Total Curies	2.58E+05	3.43E+00	3.43E-03	2.85E+07		3.54E-02	2.61E+07	2.40E+06	2.00E-02	1.65E+04
Chemicals (MT)										
Ag+	8.13E-04	3.82E-08	3.82E-11	3.15E-01		8.99E-10		3.15E-01		
Am+3	3.58E-06	1.68E-10	1.68E-13	1.39E-03		3.93E-12		1.39E-03		
As+5										
B+3	4.47E-05	2.10E-09	2.10E-12	1.73E-02		4.94E-11		1.73E-02		
Bar+2	2.02E-03	9.46E-08	9.47E-11	7.82E-01		2.23E-09		7.82E-01		
Bar+2										
Ru+3	1.90E-02	4.55E-07	4.56E-10	3.76E+00		1.08E-08		3.76E+00		
Ca+2	6.65E-02	1.64E-06	1.64E-09	1.35E+01		2.36E-06		1.35E+01		1.28E+03
Ca+2	1.95E-02	9.14E-07	9.15E-10	7.53E+00		2.87E-08		7.53E+00		3.94E+00
Ca+3	6.07E-03	2.85E-07	2.85E-10	2.35E+00		6.70E-09		2.35E+00		
Ca+3	3.76E-06	1.76E-10	1.76E-13	1.46E-03		4.15E-12		1.46E-03		
Ca+	7.87E-03	2.22E-07	2.22E-10	1.84E+00		2.08E-09	1.77E+00	6.46E-02	1.36E-09	3.48E-02
Ca+2	1.46E-04	6.70E-09	6.70E-12	5.56E-02		1.58E-10		5.56E-02		
Ca+3	5.67E-02	1.41E-06	1.41E-09	1.17E+01		3.33E-08		1.17E+01		
Ca+					1.74E+01				1.65E-01	2.32E+02
H+2	3.82E-06	1.79E-10	1.80E-13	1.48E-03		4.22E-12		1.48E-03		
K+	9.98E-01	4.69E-05	4.69E-08	3.87E+02		1.11E-06	1.75E+00	3.85E+02	1.34E-09	5.29E+00
La+3	4.51E-04	2.12E-08	2.12E-11	1.75E-01				1.75E-01		
Mg+2										
Mn+2	1.25E-07	5.85E-12	5.86E-15	4.84E-05		1.38E-13		4.84E-05		
Mn+4	2.24E-02	1.03E-06	1.03E-09	8.70E+00		2.48E-08		8.70E+00		
Mn+6	3.16E-13	1.33E-07	1.33E-23	5.91E-13		2.14E-14		6.12E-13		1.18E-05
Nat+	7.94E+02	3.33E-02	3.34E-05	5.44E+04	7.78E+02	6.04E-04	4.10E+02	5.47E+04	1.88E-07	7.51E+02
Ni+3	1.34E-02	6.30E-07	6.31E-10	5.21E+00		1.48E-08		5.21E+00		
Np+4	2.41E-05	1.13E-09	1.13E-12	9.31E-03		7.27E-09		9.31E-03		3.67E+00
Pr+4	1.81E-02	8.51E-07	8.52E-10	7.03E+00		2.70E-08		7.03E+00		3.84E+00
Ru+4	5.19E-05	2.44E-09	2.44E-12	2.02E-02		5.74E-11		2.02E-02		
Ru+	6.18E-07	2.90E-11	2.90E-14	2.40E-04		6.83E-13		2.40E-04		
Ru+7										
Ru+3										
Ru+3										
Se+6	5.06E-10	1.14E-16	1.15E-19	9.45E-16		3.43E-11		9.80E-10		1.89E-02
Si+4	1.19E+00	1.64E-05	1.63E-08	1.36E+02		1.36E-06		1.36E+02		
Sr+2	9.37E-04	4.40E-08	4.40E-11	3.64E-01		1.04E-09		3.64E-01		
Te+6										
UO+2	5.44E-01	7.56E-06	7.57E-09	6.25E+01		1.79E-07		6.25E+01		
Zn+2										
Al(OH)4-	1.58E+02	2.08E-03	2.08E-06	1.72E+04		4.94E-05		1.72E+04		
BO2-	8.63E-06	1.95E-12	1.96E-15	1.61E-05		5.86E-07		1.61E-05		3.22E+02
Cl-	1.22E+00	1.73E-04	1.74E-07	4.77E+02		1.01E-05		4.77E+02		1.87E+03
CO3-2	3.71E+00	1.74E-04	1.74E-07	1.44E+03		1.48E-03		1.44E+03		
Cr(OH)4-	3.78E+00	1.37E-04	1.37E-07	1.13E+03		3.23E-06		1.13E+03		
F-	2.67E+00	1.25E-04	1.25E-07	1.03E+03		6.32E-06		1.03E+03		1.87E+03
I-	2.31E-04	1.09E-08	1.09E-11	9.08E-02		1.67E-08		9.08E-02		9.08E+00
N2-	1.08E+02	6.97E-04	6.98E-07	5.76E+03	5.00E-04	1.67E-05	5.00E-04	5.76E+03		
NO3-	2.56E+02	3.60E-02	3.60E-05	9.91E+04	1.08E+03	6.92E-04	1.07E+03	9.91E+04	1.02E+01	7.19E+03
OH-	4.60E+02	1.50E-03	1.50E-06	1.24E+04	5.75E+02	3.17E-05	1.33E+01	1.29E+04		1.08E+02
PO4-3	1.96E+01	6.93E-04	6.93E-07	5.73E+03		1.90E-05		5.73E+03		1.49E+03
SO4-2	1.10E+01	5.15E-04	5.16E-07	4.26E+03		1.22E-05		4.26E+03		
TO4-	4.11E-03	1.93E-07	1.93E-10	1.59E+00		9.63E-09		1.59E+00		1.61E+03
H2O	2.04E+05	5.73E+05	6.39E+03	2.76E+05	7.00E+04	1.36E+04	7.35E+03	3.52E+05	6.87E+02	6.65E+05
Separable Organic	2.01E-01					6.47E-10		6.47E-10		
Organic Carbon:	8.67E-01	1.57E-04	1.57E-07	3.36E+02		3.08E-06		3.36E+02		
ZrO2·2H2O	1.94E-02	9.08E-07	9.09E-10	7.51E+00		2.14E-08		7.51E+00		

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
LIQUID COMPONENTS										
Chemicals Continued (MT)										
Hg	3.58E-09	8.10E-16	8.11E-19	6.70E-09		2.43E-10		6.94E-09		2.90E-07
TCO2	1.73E-12		3.92E-22	3.24E-12		1.18E-13		3.35E-12		6.43E-05
Cl2									2.36E+02	
CO										
CO2										
F2										
H2										
I2										
N2										
N2O										
NO										
NO2										
O2										
SO2										
Glycolic Acid	7.79E-08	1.76E-14	1.76E-17	1.46E-07		5.29E-09		1.51E-07		
H2S										
Glycolic Acid										
Kerosene										
NI3										
Polyelectrolyte	2.53E+00	2.52E-06	2.52E-09	2.08E+01		6.73E-08		2.08E+01		
Sulfur										

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Total Mass Flow (MT)	1.79E+04			2.38E+02	6.15E+02			8.52E+02		1.60E+04
Radionuclides (Ci)										
Am-241	6.03E+04			8.03E+02				8.03E+02		2.35E+02
C-14	2.07E+03			2.75E+01				2.75E+01		
Cs-137	5.25E+06			7.01E+04				7.01E+04		2.35E+04
Ba-137	4.99E+06			6.66E+04				6.66E+04		2.23E+04
Np-237	6.19E+01			8.25E-01				8.25E-01		3.48E-02
Ru-239	2.09E+04			2.78E+02				2.78E+02		6.06E+01
Ru-240	6.19E+03			8.25E+01				8.25E+01		1.69E+01
Pu-241	6.86E+04			9.14E+02				9.14E+02		2.10E+02
Sr-90	4.22E+07			5.62E+05				5.62E+05		5.36E+04
Y-90	6.22E+07			5.62E+05				5.62E+05		5.36E+04
Tc-99	8.76E+03			1.17E+02				1.17E+02		6.95E+02
Total Curies	9.48E+07			1.26E+06				1.26E+06		1.54E+05
Chemicals (MT)										
Ag+	5.49E-01			7.31E-03				7.31E-03		
Al+3	1.80E+03			2.40E+01				2.40E+01		
Am+3	1.76E-02			2.34E-04				2.34E-04		
As+5										
Be+2										
Be+2										
Bi+3	2.53E+02			3.40E+00				3.40E+00		
Ca+2	1.28E+02			1.70E+00				1.70E+00		2.56E+02
CaH2	2.34E+00			3.11E-02				3.11E-02		
Ca+3	2.32E+02			3.09E+00				3.09E+00		
Cr+3	5.64E-06			7.51E-08				7.51E-08		
Co+3										
Co+3	2.78E+02			3.70E+00				3.70E+00		
Cr+	1.74E-01			2.32E-03				2.32E-03		
Cr+2										
Fe+3	1.10E+03			1.46E+01				1.46E+01		
Hg+2	8.70E-02			1.16E-03				1.16E-03		
K+	2.69E+01			3.58E-01				3.58E-01		
La+3	2.10E+01			2.79E-01				2.79E-01		
Mg+2	1.10E+00			1.47E-02				1.47E-02		
Mn+4	1.74E+02			2.32E+00				2.32E+00		
Mn+6	1.61E-02			2.15E-04				2.15E-04		
Na+	1.23E+03			1.66E+01				1.66E+01		
NH+3	2.00E+02			2.66E+00				2.66E+00		
Np+4	8.78E-02			1.17E-03				1.17E-03		4.93E-05
Fe+4	2.62E+01			3.49E-01				3.49E-01		
Pu+4	3.65E-01			4.86E-03				4.86E-03		
Rh+3	2.92E-02			3.90E-04				3.90E-04		
Se+6	2.72E+00			3.62E-02				3.62E-02		
Si+4	4.68E+02			6.23E+00				6.23E+00		
Sr+2	3.57E+01			4.75E-01				4.75E-01		
Ti+4	2.49E+00			3.32E-02				3.32E-02		
Ti+4										
UD2+2	1.55E+03			2.07E+01				2.07E+01		
Zn+2	3.42E-01			4.53E-03				4.53E-03		
Cl-	8.78E+00			1.17E-01				1.17E-01		4.76E+00
ClO3-2	1.12E+01			1.22E+00				1.22E+00		
F-	6.71E+01			8.94E-01				8.94E-01		1.63E+02
I-	1.02E-03			1.36E-05				1.36E-05		3.71E-03
NO2-	5.86E+01			7.84E-01				7.84E-01		
NO3-	9.72E+02			1.30E+01				1.30E+01		
OH-	7.42E+03			9.90E+01				9.90E+01		2.04E-14
PO4-3	1.75E+02			2.33E+00				2.33E+00		
SO4-2	5.03E+02			1.37E+00				1.37E+00		
TeO4-	8.53E-01			1.14E-02				1.14E-02		
H2O										
MIX										7.35E-01
Organic Carbon	8.19E+01			1.09E+00				1.09E+00		
ZrO2·2H2O	1.17E+03			1.56E+01				1.56E+01		
Ag2O										1.46E-02
AlFO4										3.09E+02
Al2O3										1.74E+03
Am2O3										7.52E-05
B2O3					6.23E+00			6.23E+00		7.79E+02
BaO										3.68E-02
BaSO3										3.37E-01
CaO					4.45E-01			4.45E-01		6.23E+02

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	11	12	13	14	15	16	17	18	19	20
SOLID COMPONENTS										
Chemicals Continued (MT)										
CaO										3.65E-01
Ca2O3										2.69E-01
Ca2O3										3.47E-09
Ca2O3										6.64E-05
Ca2O3										3.04E+01
Ca2O										2.99E-03
CaO										2.93E-03
Fe2O3										1.59E+00
H2										2.73E-03
H2O										1.15E-06
K2O										1.96E+01
La2O3										2.22E-02
Li2O					2.22E+00			2.22E+00		9.36E-02
MgO					4.45E-01			4.45E-01		1.98E-02
MnO										2.63E-06
Mn2O3										1.36E-05
Na2O										3.11E+03
Na2O3										4.67E-01
Na2O										3.59E-01
Na2O										1.22E-03
Na2O										1.11E-05
Na2O3										2.03E-05
Na2O										2.46E-03
SiO2					3.11E+01			3.11E+01		6.89E+03
SiO										1.44E+01
SiO										4.17E-02
Ta2O7										6.44E-02
TiO2										1.59E-03
UD3										3.72E+00
ZnO										2.39E-04
ZnO2										7.53E-01
Consent										
Flyash										
Polyelectrolyte	1.65E+02			1.64E+00				1.64E+00		5.74E+02
CS-100 - Na Form					5.74E+02					

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30	
LIQUID COMPONENTS											
Total Mass Flow (MT)	8.23E+05	9.96E+03	4.04E+05	3.54E+06			4.01E+05	3.45E+06	2.56E+05	1.73E+04	2.79E+05
Volume (L)	6.23E+08	9.63E+06	2.62E+08	3.54E+09			4.01E+08	3.44E+09	2.52E+08	1.73E+07	2.67E+08
Specific Gravity	1.00E+00	1.00E+00	1.53E+00	1.00E+00			1.00E+00	1.00E+00	1.02E+00	1.00E+00	1.04E+00
Radionuclides (Ci)											
Am-241	1.03E-03	1.03E-06	4.76E+03						1.61E-06		
C-14	6.20E-04	6.20E-07	2.87E+03				2.90E+03		9.66E-07		
Cs-137	1.60E-01	1.60E-04	7.78E+05						1.21E-02		9.90E+05
Re-137	1.60E-01	1.60E-04	7.39E+05						1.15E-02		2.76E+05
Np-237	5.59E-04	5.60E-07	2.59E+03				2.76E+05		5.61E-07		2.58E+03
Ru-239	2.50E-04	2.51E-07	1.16E+03				2.59E+03		3.91E-07		
Ru-240	6.88E-05	6.89E-08	3.19E+02						1.00E-07		
Ru-241	8.78E-04	8.79E-07	4.07E+03						1.37E-06		
Sr-90	1.53E-01	1.53E-04	7.10E+05						2.39E-04		
Y-90	1.53E-01	1.53E-04	7.10E+05						2.39E-04		
Tc-99	7.10E-03	7.10E-06	3.29E+04				1.65E+04		9.09E-06		1.65E+04
Total Curies	6.44E-01	6.45E-04	2.98E+06				5.88E+05		2.41E-02		5.83E+05
Chemicals (MT)											
Ag+	6.81E-08	6.82E-11	3.15E-01						1.06E-10		
Am3	3.00E-10	3.00E-13	1.39E-03						4.68E-13		
As+5											
B+3	3.74E-09	3.74E-12	1.73E-02						5.84E-12		
Be+2	1.69E-07	1.69E-10	7.82E-01						2.64E-10		
Be+2											
Bi+3	8.12E-07	8.13E-10	3.76E+00						1.27E-09		
Ca+2	2.79E-04	2.79E-07	1.29E+03						2.81E-07		1.28E+03
CH2	2.48E-06	2.48E-09	1.13E+01				3.94E+00		3.40E-09		3.94E+00
Co+3	5.06E-07	5.06E-10	2.33E+00						7.93E-10		
Co+3	3.14E-10	3.15E-13	1.46E-03						4.91E-13		
Co+3	2.13E-08	2.13E-11	9.94E-02				3.46E-02		1.60E-09		3.46E-02
Cr+2	1.23E-08	1.23E-11	5.54E-02						1.86E-11		
Fe+3	2.52E-06	2.52E-09	1.17E+01						3.94E-09		
H+											
Hg+2	3.20E-10	3.20E-13	1.46E-03						1.63E-01		2.32E+02
K+	8.43E-05	8.44E-08	3.91E+02				5.29E+00		5.00E-13		5.29E+00
La+3	3.76E-08	3.78E-11	1.75E-01						1.33E-07		
La+3									5.90E-11		
Mg+2											
Mn+2	1.04E-11	1.05E-14	4.84E-05						1.63E-14		
Mn+4	1.88E-06	1.89E-09	8.70E+00						2.94E-09		
Mn+6	2.54E-12	2.55E-15	1.18E-05						2.55E-15		1.18E-05
Na+	3.76E-02	3.79E-05	5.53E+04	5.56E-01			1.18E-05		7.14E-05		7.51E+02
Ni+3	1.12E-06	1.13E-09	5.21E+00				3.01E+02		1.76E-09		
Np+5	7.94E-07	7.94E-10	3.68E+00						7.93E-10		3.67E+00
Pb+4	2.35E-06	2.35E-09	1.09E+01				3.84E+00		3.20E-09		3.84E+00
Pu+4	4.35E-09	4.35E-12	2.02E-02						6.79E-12		
Rb+	5.17E-11	5.18E-14	2.40E-04						8.08E-14		
Rb+7											
Rh+3											
Ru+3											
Sr+6	4.07E-09	4.07E-12	1.89E-02				1.89E-02		4.07E-12		1.89E-02
Si+4	2.93E-05	2.94E-08	1.36E+02						4.58E-08		
Sn+2	7.85E-08	7.86E-11	3.64E-01						1.23E-10		
Tert											
Ti+2	1.35E-05	1.35E-08	6.25E+01						2.11E-08		
Zn+2											
Al(OH)4-	3.71E-03	3.72E-06	1.72E+04						5.80E-06		
BiO2-	6.95E-05	6.95E-08	3.22E+02				3.22E+02		6.93E-08		3.22E+02
Cl-	1.02E-03	1.02E-06	2.33E+03						1.19E-06		1.87E+03
CO3-2									1.74E-07		
Cr(OH)4-	2.44E-04	2.44E-07	1.13E+03						3.81E-07		
F-	6.26E-04	6.27E-07	2.90E+03						7.52E-07		1.87E+03
I-	1.93E-06	1.93E-09	9.17E+01				9.08E+03		1.93E-09		9.08E+03
NO2-	1.24E-03	1.25E-06	5.76E+03						1.94E-06		
NO3-	4.59E-02	4.59E-05	1.06E+05						1.02E+01		7.19E+03
OH-	8.23E+03	2.09E-06	9.67E+03				4.33E+02	7.19E+03	2.23E+02		1.08E+02
PO4-3	1.55E-03	1.56E-06	7.20E+03	4.11E-01			1.49E+03		2.25E-06		1.49E+03
SO4-2	9.19E-04	9.20E-07	4.26E+03						1.44E-06		
TOC+	6.91E-07	6.92E-10	3.20E+00						8.83E-10		1.61E+00
H2O	8.23E+05	9.14E+03	1.89E+05	4.31E+05			4.01E+05	2.30E+05	1.62E+04		2.64E+05
Separable Organic	1.40E-16	1.40E-19	6.47E-10					6.74E+04			
Organic Carbon	2.07E-04	2.08E-07	3.36E+02						1.45E-19		3.63E-07
ZrO2·2H2O	1.62E-06	1.62E-09	7.51E+00						2.53E-09		

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
LIQUID COMPONENTS										
Chemicals Continued (MT)										
H ₂	6.42E-14	6.42E-17	2.97E-07				2.62E-03		6.50E-17	2.90E-07
TCO2	1.39E-11	1.39E-14	6.45E-05				1.25E+00		1.39E-14	6.45E-05
Cl2										
CO		8.20E+02					2.93E+03		1.06E+03	
CO2										
F2										
H2										
I2										
N2				2.46E+06			2.48E+06	1.40E+05		
N2O										
NO							1.37E+02			
NO2							8.37E+02			
O2				6.53E+05			7.26E+05	3.73E+04		
SO2							2.57E+03			
Glycolic Anion	3.26E-14	3.26E-17	1.51E-07						5.02E-17	
H2S										
Glycolic Acid										
Kerosene								1.00E+01		
NE3								3.65E+03		
Polyelectrolyte	4.50E-06	4.50E-09	2.08E+01						7.03E-09	
Sulfur										

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
SOLID COMPONENTS										
Total Mass Flow (MT)			1.68E+04	2.77E+05	3.69E+05	7.50E+03	8.07E+03	5.58E+03		8.45E+03
Radionuclides (Ci)										
Am-241			1.04E+03		5.57E+03	1.13E+02	1.22E+02			1.22E+02
C-14			2.75E+01							
Cs-137			9.36E+04		5.58E+05	1.13E+04	1.22E+04			1.22E+04
Ba-137			8.89E+04		5.30E+05	1.08E+04	1.16E+04			1.16E+04
Np-237			8.60E-01		8.25E-01	1.69E-02	1.80E-02			1.80E-02
Pu-239			3.97E+02		1.44E+03	2.92E+01	3.14E+01			3.14E+01
Pu-240			9.94E+01		4.01E+02	8.15E+00	8.77E+00			8.77E+00
Pu-241			1.12E+03		4.98E+03	1.01E+02	1.09E+02			1.09E+02
Sr-90			6.16E+05		1.27E+06	2.58E+04	2.78E+04			2.78E+04
Y-90			6.16E+05		1.27E+06	2.58E+04	2.78E+04			2.78E+04
Tc-99			8.12E+02		1.65E+04	3.35E+02	3.60E+02			3.60E+02
Total Curies			1.42E+06		3.66E+06	7.43E+04	8.00E+04			8.00E+04
Chemicals (MT)										
As+			7.31E-03							
Al+3			2.40E+01							
Am+3			2.34E-04							
As+5										
Be+2										
Be+2										
Bi+3			3.40E+00					1.47E+03		2.56E+02
Ca+2			2.58E+02							
Ca+2			3.11E-02							
Ca+3			3.09E+00							
Ca+3			7.51E-08							
Co+3			3.70E+00							
Co+3			2.32E-03							
Cs+										
Cr+2										
Fe+3			1.46E+01							
Fe+2			1.16E-03							
K+			3.58E-01							
La+3			2.79E-01							
Mg+2			1.47E-02							
Mg+2			2.32E+00							
Mn+6			2.15E-04							
Na+			1.66E+01							
Ni+3			2.66E+00							
Np+4			1.22E-03		1.17E-03	2.38E-05	2.56E-05			2.56E-05
Pb+4			3.49E-01							
Pu+4			4.86E-03							
Pu+3			3.50E-04							
Se+6			3.62E-02							
Si+4			6.23E+00							
Sn+2			4.73E-01							
Ti+4			3.32E-02							
Ti+4										
UD2+2			2.07E+01							
Zn+2			4.53E-03							
Cl-			4.89E+00		1.13E+02	2.30E+00	2.47E+00			2.47E+00
CO3-2			1.22E+00							
F-			1.63E+02		9.82E+02	2.00E+01	2.15E+01			1.43E+02
I-			3.73E-03		8.80E-02	1.79E-03	1.92E-03			1.92E-03
NO2-			7.84E-01							
NO3-			1.30E+01							
OH-			9.90E+01					1.24E+03		2.04E-14
FO4-3			2.33E+00							
SO4-2			1.37E+00							
TiO4-			1.14E-02							
H2O			7.35E-01		1.74E+01	3.54E-01	3.81E-01			3.81E-01
HCl2			1.09E+00							
Organic Carbon			1.56E+01							
ZrO2·2H2O			1.46E-02		3.47E-01	7.04E-03	7.58E-03			7.58E-03
Ag2O			3.09E+02		7.94E+03	1.49E+02	1.60E+02			1.60E+02
Al(OH)3			1.74E+03	3.50E+04	4.13E+04	8.38E+02	9.01E+02			9.01E+02
Am2O3			7.52E-05		1.78E-03	3.62E-05	3.90E-05			3.90E-05
B2O3			7.83E+02	1.85E+04	1.85E+04	3.79E+02	4.04E+02			4.04E+02
B2O			3.68E-02		8.73E-01	1.77E-02	1.91E-02			1.91E-02
Bi2O3			3.37E-01		7.98E+00	1.62E-01	1.74E-01			1.74E-01
CaO			6.23E+02	1.26E+04	1.48E+04	3.00E+02	3.23E+02			3.23E+02

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	21	22	23	24	25	26	27	28	29	30
SOLID COMPONENTS										
Chemicals Continued (MT)										
CaO			3.65E-01		8.66E+00	1.76E-01	1.89E-01			1.89E-01
Ca2O3			2.69E-01		6.37E+00	1.30E-01	1.39E-01			1.39E-01
Ca2O3			3.47E-09		8.24E-08	1.67E-09	1.80E-09			1.80E-09
Ca2O3			8.64E-05		2.03E-03	4.16E-05	4.48E-05			4.48E-05
Ca2O3			3.04E+01		7.22E+02	1.47E+01	1.58E+01			1.58E+01
Ca2O			2.99E-03		7.08E-02	1.44E-03	1.52E-03			1.52E-03
CaO			2.93E-03		6.96E-02	1.41E-03	1.52E-03			1.52E-03
Fe2O3			1.59E+00		3.76E+01	7.64E-01	8.22E-01			8.22E-01
Hg			2.73E-03		2.62E-03	5.31E-05	5.72E-05			2.67E-03
HgO			1.15E-06		2.74E-05	5.56E-07	5.98E-07			5.98E-07
K2O			1.96E+01		4.63E+02	9.44E+00	1.02E+01			1.02E+01
La2O3			2.22E-02		5.33E-01	1.08E-02	1.16E-02			1.16E-02
Li2O			2.32E+00		2.22E+00	4.52E-02	4.86E-02			4.86E-02
MgO			4.69E-01		4.69E-01	9.53E-03	1.03E-02			1.03E-02
MnO			2.63E-06		6.24E-05	1.27E-06	1.36E-06			1.36E-06
Mn2O3			1.36E-05		3.22E-04	6.54E-06	7.04E-06			7.04E-06
N2O			3.11E+03		7.99E+04	1.50E+03	1.61E+03			1.61E+03
Ni2O3			4.67E-01		1.11E+01	2.25E-01	2.42E-01			2.42E-01
NiO2			3.59E-01		8.32E+00	1.73E-01	1.86E-01			1.86E-01
NiO			1.23E-03		2.94E-02	5.76E-04	6.23E-04			6.23E-04
Ni2O			1.11E-05		2.62E-04	5.32E-06	5.73E-06			5.73E-06
Ni2O3			2.03E-05		4.80E-04	9.76E-06	1.05E-05			1.05E-05
SnO3			2.66E-03		5.83E-02	1.18E-03	1.27E-03			1.27E-03
SnO2			8.52E+03	2.10E+05	2.11E+05	4.28E+03	4.61E+03			4.61E+03
SnO			1.44E+01		3.42E+02	6.95E+00	7.47E+00			7.47E+00
SiO			4.17E-02		9.88E-01	2.01E-02	2.16E-02			2.16E-02
Ta2O7			6.44E-02		1.53E+00	3.10E-02	3.34E-02			3.34E-02
Ta2O5			1.59E-03		3.77E-02	7.67E-04	8.23E-04			8.23E-04
UO3			3.72E+00		8.81E+01	1.79E+00	1.93E+00			1.93E+00
ZnO			2.39E-04		5.67E-03	1.15E-04	1.24E-04			1.24E-04
ZnO2			7.53E-01		1.79E+01	3.63E-01	3.90E-01			3.90E-01
Amant								1.44E+03		
Flyash								1.44E+03		
PolysElectrolyte			1.64E+00							
CS-100 - Na Foam			5.74E+02							

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
LIQUID COMPONENTS										
Total Mass Flow (MT)	3.44E+06	1.15E+03			5.86E+02	2.20E+03	1.62E+05	1.79E+03	4.43E+04	9.77E+03
Volume (L)	3.44E+09	1.15E+06			5.86E+05	2.20E+06	1.62E+08	1.79E+06	4.30E+07	9.77E+06
Specific Gravity	1.00E+00	1.00E+00			1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.03E+00	1.00E+00
Radionuclides (Ci)										
Am-241	1.61E-06					6.07E-04	4.69E-06	4.70E-09	1.23E+01	
C-14	2.90E+03					3.66E-04	2.83E-06	2.83E-09	7.40E+00	
Cs-137	1.36E-02					6.68E+02	5.02E-02	5.02E-05	1.31E+05	
Ha-137	1.29E-02					6.35E+02	4.77E-02	4.77E-05	1.25E+05	
Np-237	1.33E-05					1.63E-02	1.28E-08	1.28E-11	3.33E-02	
Ru-239	3.91E-07					1.48E-04	1.14E-06	1.15E-09	2.99E+00	
Ru-240	1.00E-07					4.07E-05	3.15E-07	3.15E-10	8.22E-01	
Ru-241	1.37E-06					5.19E-04	4.01E-06	4.01E-09	1.05E+01	
Sr-90	2.39E-04					9.06E-02	7.00E-04	7.01E-07	1.83E+03	
Y-90	2.39E-04					9.06E-02	7.00E-04	7.01E-07	1.83E+03	
Tc-99	9.13E-05					4.37E-01	1.63E-05	1.63E-08	4.27E+01	
Total Curies	3.48E+03					1.30E+03	9.92E-02	9.93E-05	2.59E+05	
Chemicals (MT)										
Ag+	1.06E-10					4.03E-08	3.11E-10	3.11E-13	8.13E-04	
Am+3	4.66E-13					1.77E-10	1.37E-12	1.37E-15	3.56E-06	
BH3	5.84E-12					2.21E-09	1.71E-11	1.71E-14	4.47E-05	
Ba+2	2.64E-10					9.98E-08	7.71E-10	7.72E-13	2.02E-03	
Ba+2					1.02E-10	9.39E-07	7.26E-09	7.26E-12	1.90E-02	
Ba+3	1.27E-09					3.29E-06	2.54E-08	2.55E-11	6.63E-02	
Ca+2	2.81E-07					9.64E-07	7.43E-09	7.43E-12	1.93E-02	
CH2	2.31E-08					3.00E-07	2.32E-09	2.32E-12	6.07E-03	
Ca+3	7.93E-10									
Ca+3	4.91E-13					1.86E-10	1.44E-12	1.44E-15	3.76E-06	
Ca+2	1.78E-09					8.81E-05	3.04E-09	3.05E-12	7.96E-03	
Ca+2	1.86E-11					7.10E-09	5.48E-11	5.49E-14	1.43E-04	
Fe+3	3.94E-09					2.81E-06	2.17E-08	2.17E-11	5.67E-02	
H+	1.63E-01					2.92E-05				
Hg+2	5.00E-13					1.89E-10	1.46E-12	1.46E-15	3.82E-06	
K+	1.59E-07					1.36E-04	3.82E-07	3.82E-10	9.90E-01	
La+3	5.90E-11					2.23E-08	1.73E-10	1.73E-13	4.51E-04	
Mg+2										
Mg+2	1.63E-14					6.17E-12	4.77E-14	4.77E-17	1.25E-07	
Mn+4	2.94E-09					1.11E-06	8.39E-09	8.39E-12	2.24E-02	
Mn+6	6.14E-14							1.21E-22	3.16E-13	
Na+	7.52E-05					5.96E-02	4.13E-04	4.13E-07	7.94E+02	
NH3	1.76E-09					6.64E-07	5.13E-09	5.14E-12	1.34E-02	
Np+4	1.92E-08					2.32E-05	1.81E-11	1.81E-14	4.73E-05	
Et+4	2.24E-08					8.98E-07	6.94E-09	6.94E-12	1.81E-02	
Pu+4	6.79E-12					2.57E-09	1.99E-11	1.99E-14	5.20E-05	
Rb+	8.05E-14					3.06E-11	2.36E-13	2.37E-16	6.18E-07	
Ru+7										
Ru+3										
Ru+3										
Sa+6	9.83E-11					2.50E-14	1.93E-16	1.94E-19	5.06E-10	
Si+4	4.58E-08					5.91E-05	4.57E-07	4.57E-10	1.19E+00	
Sn+2	1.23E-10					4.64E-08	3.59E-10	3.59E-13	9.37E-04	
Te+6										
Te+2	2.11E-08					2.70E-05	2.08E-07	2.08E-10	5.44E-01	
Zn+2										
Al(OH)4-	5.80E-06					7.84E-03	6.06E-05	6.06E-08	1.58E+02	
Br2	1.66E-06					4.27E-10	3.30E-12	3.31E-15	8.63E-06	
Cl-	1.24E-05					6.18E-05	9.42E-07	9.43E-10	1.23E+00	
CO3-2	1.74E-07					1.28E-09	1.42E-06	1.42E-09	3.71E+00	
Cr(OH)4-	3.81E-07					1.87E-04	1.43E-06	1.43E-09	3.78E+00	
F-	1.10E-05					1.32E-04	1.02E-06	1.02E-09	2.67E+00	
I-	4.74E-08					1.15E-08	8.85E-11	8.86E-14	2.31E-04	
NO2-	1.94E-06					2.66E-03	4.12E-05	4.12E-08	1.08E+02	
NO3-	1.02E+01					6.63E-02	1.96E-04	1.96E-07	2.56E+02	
OH-	3.59E-06					1.38E-07	1.76E-04	1.76E-07	4.60E+02	
IO4-3	6.69E-06					9.71E-04	7.40E-06	7.41E-09	1.93E+01	
SO4-2	1.44E-06					1.17E-03	4.20E-06	4.20E-09	1.10E+01	
TO4-	8.85E-10					4.24E-05	1.59E-09	1.59E-12	4.15E-03	
H2O	1.22E+04					1.52E+05	1.75E+03	1.75E+04	4.23E+04	
Separable Organic	1.40E-19					9.93E-06	7.67E-08	7.68E-11	2.01E-01	2.01E+03
Organic Carbon	3.65E-07					3.00E-04	9.47E-07	9.48E-10	8.67E-01	
Zr(O)2:H2O	2.53E-09					9.58E-07	7.40E-09	7.41E-12	1.94E-02	

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
LIQUID COMPONENTS										
Chemicals Continued (MT)										
Hg	1.53E-08						1.37E-15	1.37E-18	3.58E-09	
TcO2	6.45E-09									
Cl2										
CO	2.04E+01									
CO2	3.98E+03									
F2										
H2	1.87E+02									
I2										
NE2	2.62E+06									
N2O										
NO	1.37E+00									
N2	1.04E+01									
O2	7.61E+05									2.95E+03
SO2	2.57E+02									
Glycolic Acid	5.02E-17					1.64E+00	6.27E-07	6.27E-10	1.64E+00	
HES	8.99E+00									4.81E+03
Glycolic Acid										
Kerosene										
NE3	3.75E+01									
Polyelectrolyte	7.03E-09					1.25E-04	9.69E-07	9.70E-10	2.53E+00	
Sulfur		1.15E+03								

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
SOLID COMPONENTS										
Total Mass Flow (MT)	1.87E-01		5.74E+03			4.22E+00			1.79E+04	6.77E+04
Radionuclides (Ci)										
Am-241	2.81E-03					2.99E+00			6.03E+04	
C-14						1.02E-01			2.07E+03	
Cs-137	2.82E-01					2.62E+02			5.25E+06	
Ba-137	2.68E-01					2.49E+02			4.99E+06	
Np-237	4.17E-07					3.07E-03			6.15E+01	
Pu-239	7.27E-04					1.04E+00			2.09E+04	
Pu-240	2.03E-04					3.07E-01			6.19E+03	
Pu-241	2.52E-03					3.40E+00			6.86E+04	
Sr-90	6.43E-01					2.03E+03			4.22E+07	
Y-90	6.43E-01					2.09E+03			4.22E+07	
Tc-99	8.34E-03					4.67E-01			8.76E+03	
Total Curies	1.85E+00					4.71E+03			9.48E+07	
Chemicals (MT)										
Ag+						2.72E-05			5.49E-01	
Al+3						8.89E-02			1.80E+03	
Am+3						8.70E-07			1.76E-02	
As+5										
Ba+2										
Ba+2										
Bi+3						1.26E-02			2.55E+02	
Ca+2			1.17E+02			6.33E-03			1.23E+02	
Ca+2						1.43E-03			2.34E+00	
Ca+2						1.15E-02			2.32E+02	
Ca+3						2.79E-10			5.64E-06	
Co+3										
Co+3						1.38E-02			2.79E+02	
Co+3						8.60E-06			1.74E-01	
Co+										
Cr+2										
Cr+2						5.43E-02			1.10E+03	
Hg+2						4.31E-06			8.70E-02	
K+						1.33E-03			2.69E+01	
La+3						1.04E-03			2.10E+01	
Mg+2						5.45E-05			1.10E+00	
Mn+4						8.61E-03			1.74E+02	
Mn+6						7.98E-07			1.61E-02	
Ni+						6.17E-02			1.25E+03	
Ni+3						9.88E-03			2.06E+02	
Np+4						4.36E-06			8.78E-02	
Pb+4						1.30E-03			2.62E+01	
Pu+4						1.81E-05			3.65E-01	
Rn+3						1.45E-06			2.93E-02	
Se+6						1.35E-04			2.72E+00	
Si+4						2.32E-02			4.68E+02	
Sn+2						1.77E-03			3.57E+01	
Ti+4						1.23E-04			2.49E+00	
Ti+4										
UO2+2						7.69E-02			1.55E+03	
Zn+2						1.69E-05			3.42E-01	
Cl-						9.30E-04			8.73E+00	
OD3-2						4.52E-03			9.12E+01	
F-						4.47E-03			6.71E+01	
I-	4.97E-04		5.30E+01			5.07E-08			1.02E-03	
NO2-	4.45E-08					2.91E-03			5.85E+01	
NO3-						4.81E-02			9.72E+02	
OH-						3.39E-01			7.42E+03	
RO4-3						8.65E-03			1.75E+02	
SO4-2						5.11E-03			1.03E+02	
TeO4-						4.22E-05			8.53E-01	
H2O										
H2O2						2.73E-05			2.73E-05	
MO2						4.06E-03			8.19E+01	
Organic Carbon										
ZnO2.ZH2O						5.78E-02			1.17E+03	
Ag2O	1.75E-07					5.86E-08			5.86E-08	
Al(OH)3	3.71E-03					2.48E-05			2.48E-05	
Al2O3	2.09E-02					3.35E-04			3.35E-04	
Am2O3	9.01E-10					1.92E-09			1.92E-09	
B2O3	9.34E-03					8.17E-01			8.17E-01	1.63E+04
BaO	4.40E-07					2.23E-10			2.23E-10	
Bi2O3	4.04E-06					2.82E-05			2.82E-05	
CaO	7.47E-03					1.78E-05			1.78E-05	

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Table E-2 Phase 2 Mass Balance with Revised TWRS Inventory

STREAM NAME	31	32	33	34	35	36	37	38	39	40
SOLID COMPONENTS										
Chemicals Continued (MT)										
CaO	4.36E-06					2.17E-05			2.17E-05	
Ca2O3	3.22E-06					2.70E-05			2.70E-05	
Ca2O8	4.16E-14					6.13E-13			6.13E-13	
Ca2O3	1.04E-09					8.66E-13			8.66E-13	
Ca2O3	3.65E-04					4.05E-05			4.05E-05	
Cs2O	3.59E-08					6.98E-06			6.98E-06	
ClO	3.52E-08					1.78E-11			1.78E-11	
Fe2O3	1.96E-05					3.36E-03			3.36E-03	6.47E+01
Hg	1.32E-09									
HgO	1.38E-11									
K2O	2.33E-04					5.84E-06			5.84E-06	
La2O3	2.69E-07					2.44E-06			2.44E-06	
Li2O	1.13E-06					2.44E-01			2.44E-01	4.92E+03
MgO	2.37E-07					1.81E-07			1.81E-07	
MnO	3.16E-11					1.60E-14			1.60E-14	
Mn2O3	1.63E-10					1.21E-08			1.21E-08	
Na2O	3.73E-02					3.94E-02			3.94E-02	7.83E+02
Ni2O3	5.60E-06					2.79E-05			2.79E-05	
BiO2	4.31E-06					1.66E-04			1.66E-04	
PbO2	1.43E-08					4.10E-08			4.10E-08	
Rb2O	1.33E-10					6.70E-14			6.70E-14	
Rh2O3	2.43E-10					3.58E-09			3.58E-09	
SrO3	2.93E-08					2.41E-05			2.41E-05	
SiO2	1.07E-01					2.26E+00			2.26E+00	4.56E+04
SO3	1.73E-04					5.24E-06			5.24E-06	
SrO	5.00E-07					4.17E-06			4.17E-06	
Ta2O7	7.72E-07					3.08E-06			3.08E-06	
TiO2	1.91E-08					2.81E-07			2.81E-07	
UO3	4.46E-05					1.63E-04			1.63E-04	
ZnO	2.87E-09					4.22E-08			4.22E-08	
ZrO2	9.02E-06					8.97E-05			8.97E-05	
Cement			1.44E+03							
Flyash			1.44E+03							
Polyelectrolyte						8.16E-03				
CS-100 - Na Form									1.65E+02	

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Table E-2 Phase II Mass Balance with Revised TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
LIQUID COMPONENTS								
Total Mass Flow (MT)	1.97E+04		8.64E+04	2.56E+01	5.82E+04	8.20E+03	8.22E-02	1.03E+06
Volume (L)	1.96E+07		8.64E+07	2.56E+04	5.82E+07	8.20E+06	8.22E+01	1.03E+09
Specific Gravity	1.00E+00		1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00	1.00E+00
Radionuclides (Ci)								
Am-241			6.14E-04			6.14E-06		1.02E-03
C-14			2.08E+03			2.08E+03		6.16E-04
Cs-137			5.78E+02			6.73E+00		1.20E+00
Ra-137			6.41E+02			6.41E+00		1.14E+00
Np-237	3.30E+02		3.30E+02		9.89E-05	2.10E-01		3.86E-04
Ru-239			1.50E-04			1.50E-06		2.49E-04
Ru-940			4.11E-05			4.11E-07		6.84E-05
Ru-241			5.24E-04			5.24E-06		8.73E-04
Sr-90			9.15E-02			9.15E-04		1.52E-01
Y-90			9.15E-02			9.15E-04		1.52E-01
Tc-99	8.79E+03		8.83E+03		2.64E-03	5.63E+00		7.43E-03
Total Curies	9.12E+03		1.29E+04		2.73E-03	2.51E+03		2.66E+00
Chemicals (MT)								
Ag+			4.07E-08			4.07E-10		6.77E-08
Am+3			1.79E-10			1.79E-12		2.98E-10
As+5								
B+3			2.23E-09			2.23E-11		3.72E-09
Ba+2			1.01E-07			1.01E-09		1.68E-07
Be+2								
Bi+3			9.49E-07			9.49E-09		8.10E-07
Ca+2			3.32E-06			3.32E-08		1.78E-04
Ca+2			9.73E-07			9.73E-09		2.16E-06
Ca+3			3.03E-07			3.03E-09		5.05E-07
Cl+3								
Co+3			1.88E-10			1.88E-12		3.13E-10
Co+3			8.90E-05			8.90E-07		1.57E-07
Cr+2			7.17E-09			7.17E-11		1.19E-08
Fe+3			2.83E-06			2.83E-08		2.51E-06
H+	5.90E-01		2.93E-05	9.05E-06	1.77E-07	3.62E-04		
Hg+2			1.91E-10			1.91E-12		3.18E-10
K+			1.37E-04			1.37E-06		8.33E-05
La+3			2.26E-08			2.26E-10		3.79E-08
Mg+2								
Mn+2			6.23E-12			6.23E-14		1.04E-11
Mn+4			1.12E-06			1.12E-08		1.87E-06
Mn+6								1.61E-12
Na+			6.02E-02			6.02E-04		4.59E-02
Ni+3			6.71E-07			6.71E-09		1.12E-06
Np+4	4.68E-01		4.68E-01		1.40E-07	2.98E-04		5.47E-07
H+4			9.07E-07			9.07E-09		2.04E-06
Pu+4			2.60E-09			2.60E-11		4.32E-09
Ru+7			3.09E-11			3.09E-13		5.14E-11
Ru+3								
Ru+3								
Ru+3								
Se+6			2.53E-14			2.53E-16		2.58E-09
Si+4			5.97E-05			5.97E-07		2.94E-05
Si+2			4.69E-08			4.69E-10		7.80E-08
Ta+6								
UO2+2			2.72E-05			2.72E-07		1.35E-05
Zn+2								
Al(CH4)-			7.92E-03			7.92E-05		3.72E-03
BiO-			4.32E-10			4.32E-12		4.41E-05
Cl-			6.16E-05			6.16E-07		7.60E-04
CO3-2						1.42E-10		1.12E-04
Cr(CH4)-			1.89E-04			1.89E-06		2.43E-04
F-			1.33E-04			1.33E-06		4.76E-04
I-			1.16E-08			1.16E-10		1.23E-06
NO2-			2.69E-03			2.69E-05		1.26E-03
NO3-	1.86E+01		6.72E-02	5.61E-04	1.11E-05	1.25E-02		5.21E-02
OH-						1.76E-08		2.39E-03
FO4-3			9.81E-04			9.81E-06		1.43E-03
SO4-2	1.27E+01		1.18E-03		3.80E-06	8.10E-03		9.16E-04
ToO4-	8.56E-01		4.30E-05		2.57E-07	4.30E-07		7.29E-07
H2O	1.96E+04		7.86E+04	2.56E+01	5.82E+04	4.44E+02		1.03E+06
Separable Organic			1.03E-05			1.03E-07		4.88E-08
Organic Carbon			3.03E-04			3.03E-06		2.32E-04
ZnO2.ZH2O			9.68E-07			9.68E-09		1.61E-06

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Table E-2 Phase II Mass Balance with Revised TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
LIQUID COMPONENTS								
Chemicals Continued (MT)								
H ₂	9.62E-02		1.83E-01		2.86E-08	1.25E-03	8.22E-02	1.83E-08
TCO2			6.88E-01			4.38E-04		8.85E-12
CL2			2.00E-02			2.00E-02		
CO								
CO2			6.41E+03			6.41E+03		
F2			9.30E-02			9.30E-02		
H2								
I2			1.26E-03			1.26E-03		
N2			1.35E+02			1.35E+02		
N2O			1.72E+01			1.72E+01		
NO			9.12E+02			9.03E+02		
N2E								
O2			2.68E+02			2.59E+02		
SO2			4.23E+01			3.39E+01		
Glycolic Anion			1.66E+00			1.66E-02		3.98E-07
H2S								
Glycolic Acid								
Kerosene								
NH3			2.71E+00			2.71E+00		
Polyelectrolyte			1.27E-04			1.27E-06		5.07E-06
Sulfur								

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Table E-2 Phase II Mass Balance with Revised TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
SOLID COMPONENTS								
Total Mass Flow (MT)	3.39E+02	8.17E+04	3.43E+02			6.46E-08		
Radionuclides (Ci)								
Am-241	1.21E+02	6.03E+04	1.24E+02			2.68E-08		
C-14	1.03E-03		1.03E-01			2.59E-10		
Cs-137	3.76E+04	1.88E+07	3.79E+04			6.64E-06		
Ba-137	3.57E+04	1.78E+07	3.60E+04			6.31E-06		
Np-237	1.24E-01	6.19E+01	1.27E-01			2.75E-11		
Ru-239	4.19E+01	2.09E+04	4.29E+01			9.28E-09		
Ru-240	1.24E+01	6.20E+03	1.27E+01			2.75E-09		
Ru-241	1.38E+02	6.86E+04	1.41E+02			3.03E-08		
Sr-90	8.46E+04	4.22E+07	8.67E+04			1.88E-05		
Co-90	8.46E+04	4.22E+07	8.67E+04			1.88E-05		
Tc-99	6.72E+02	8.80E+03	6.73E+02			1.08E-07		
Total Curies	2.43E+05	1.21E+08	2.48E+05			5.06E-05		
Chemicals (MT)								
Ag+	2.75E-07		2.75E-05			6.86E-14		
Al+3	8.98E-04		8.98E-02			2.25E-10		
Am+3	8.78E-09		8.78E-07			2.20E-15		
As+5								
Be+2								
Be+2								
Bi+3	1.28E-04		1.28E-02			3.19E-11		
Ca+2	6.39E-05		6.39E-03			1.60E-11		
Ca+2	1.17E-06		1.17E-04			2.92E-13		
Ce+3	1.16E-04		1.16E-02			2.90E-11		
Cl-1	2.82E-12		2.82E-10			7.05E-19		
Co+3	1.39E-04		1.39E-02			3.47E-11		
Co+3	8.69E-08		8.69E-06			2.17E-14		
Cr+2								
Fe+3	5.49E-04		5.49E-02			1.37E-10		
Fe+3	4.35E-08		4.35E-06			1.09E-14		
K+	1.34E-05		1.34E-03			3.36E-12		
La+3	1.05E-05		1.05E-03			2.62E-12		
Mg+2	5.50E-07		5.50E-05			1.38E-13		
Mn+4	8.70E-05		8.70E-03			2.17E-11		
Mo+6	8.06E-09		8.06E-07			2.01E-15		
Ni+3	6.23E-04		6.23E-02			1.56E-10		
Ni+3	9.98E-05		9.98E-03			2.49E-11		
Np+4	1.76E-04	8.78E-02	1.80E-04			3.90E-14		
Hf+4	1.31E-05		1.31E-03			3.27E-12		
Ru+4	1.82E-07		1.82E-05			4.56E-14		
Ru+3	1.46E-08		1.46E-06			3.66E-15		
Se+6	1.36E-06		1.36E-04			3.40E-13		
Si+4	2.34E-04		2.34E-02			5.85E-11		
Si+2	1.78E-05		1.78E-03			4.46E-12		
Th+4	1.23E-06		1.23E-04			3.11E-13		
Ti+4								
UO2+2	7.77E-04		7.77E-02			1.94E-10		
Zn+2	1.71E-07		1.71E-05			4.27E-14		
Cl-	1.03E+01	1.00E+01	1.03E+01			1.89E-09		
ClO2-2	4.56E-05		4.56E-03			1.14E-11		
F-	2.32E+01	6.97E+01	2.32E+01			3.71E-09		
I-	5.12E-10		5.12E-08			1.28E-16		
NO2-	2.94E-05		2.94E-03			7.35E-12		
NO3-	4.86E-04		4.86E-02			1.22E-10		
OH-	3.42E-03		3.42E-01			8.56E-10		
FO3-	8.74E-05		8.74E-03			2.18E-11		
SO4-2	5.16E-05		5.16E-03			1.29E-11		
TeO4-	4.26E-07		4.26E-05			1.07E-13		
H2O								
NH3	5.52E-01	2.75E+02	5.52E-01			8.79E-11		
Organic Carbon	4.10E-05		4.10E-03			1.02E-11		
ZnO2.2H2O	5.84E-04		5.84E-02			1.46E-10		
Ag2O	1.18E-03	5.91E-01	1.18E-03			1.89E-13		
Al(OH)3	5.03E-01	2.50E+02	5.03E-01			7.97E-11		
Al2O3	6.76E+00	3.37E+03	6.76E+00			1.08E-09		
Am2O3	3.87E-05	1.93E-02	3.87E-05			6.17E-15		
B2O3	1.63E+02	1.63E+04	1.66E+02			2.83E-08		
B4O7	4.51E-06	2.25E-03	4.51E-06			7.18E-16		
BL2O3	5.70E-01	2.84E+02	5.70E-01			9.08E-11		
CaO	5.59E-01	1.79E+02	5.59E-01			5.71E-11		

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Table E-2 Phase II Mass Balance with Revised TWRS Inventory

STREAM NAME	41	42	43	44	45	46	47	48
SOLID COMPONENTS								
Chemicals Continued (MT)								
CdO	4.38E-01	2.69E+00	4.38E-01				6.98E-11	
CaO ₂	5.44E-01	2.72E+02	5.44E-01				8.67E-11	
Ca ₂ O ₃	1.24E-08	6.18E-06	1.24E-08				1.97E-18	
Ca ₂ SO ₄	2.75E-08	5.28E-06	1.75E-08				2.79E-18	
Ca ₂ CO ₃	8.19E-01	4.09E+02	8.19E-01				1.33E-10	
Ca ₂ O	1.41E-01	2.07E+00	1.41E-01				2.25E-11	
CaO	3.60E-07	1.79E-04	3.60E-07				5.73E-17	
Fe ₂ O ₃	3.28E+00	1.63E+03	3.28E+00				5.30E-10	
H ₂								
H ₂ O								
K ₂ O	1.18E-01	3.57E+01	1.18E-01				1.88E-11	
La ₂ O ₃	4.93E-02	2.46E+01	4.93E-02				7.85E-12	
Li ₂ O	9.86E+00	4.82E+03	1.01E+01				2.19E-09	
MgO	3.66E-03	1.82E+00	3.66E-03				5.82E-13	
MnO	3.23E-10	1.61E-07	3.23E-10				5.14E-20	
N ₂ O ₃	2.44E-04	2.42E-02	2.44E-04				3.89E-14	
Na ₂ O	1.35E+01	4.09E+03	1.36E+01				2.25E-09	
Ni ₂ O ₃	5.63E-01	2.81E+02	5.63E-01				8.97E-11	
NiO ₂	3.36E+00	3.02E+01	3.36E+00				5.35E-10	
NiO	8.25E-04	4.14E-01	8.25E-04				1.32E-13	
Rb ₂ O	1.35E-09	6.76E-07	1.35E-09				2.16E-19	
Rb ₂ O ₃	7.23E-05	3.61E-02	7.23E-05				1.15E-14	
SeO ₃	4.86E-01	4.37E+00	4.86E-01				7.74E-11	
SiO ₂	9.34E+01	4.66E+04	9.52E+01				2.06E-08	
SO ₃	1.06E-01	5.28E+01	1.06E-01				1.69E-11	
SiO	8.42E-02	4.20E+01	8.42E-02				1.34E-11	
Ti ₂ O ₃	6.22E-02	8.14E-01	6.22E-02				9.91E-12	
TiO ₂	5.68E-03	2.83E+00	5.68E-03				9.04E-13	
UO ₂	3.30E+00	1.65E+03	3.30E+00				5.26E-10	
ZnO	8.53E-04	4.26E-01	8.53E-04				1.36E-13	
Zn ₂ CO ₃	1.81E+00	9.04E+02	1.81E+00				2.89E-10	
Cement Flyash Polyelectrolyte CS-100 - Na Form	8.24E-05		8.24E-03				2.06E-11	

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APPENDIX F ASSUMPTIONS AND BASES

Westinghouse
Hanford Company

TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE

Internal
Memo

From: Process Technology
 Phone: 373-2641 H5-27
 Date: May 7, 1996
 Subject: TWRS PROCESS TECHNICAL BASELINE ASSUMPTIONS AND BASES

73510-96-014

To: J. O. Honeyman G3-21

cc: J. N. Appel G3-21
 J. S. Garfield* H5-49
 K. A. Gasper* G3-21
 M. E. Johnson G3-21
 R. A. Kirkbride H5-27 *RAK*
 E. J. Kosiancic* H5-61 *EJK*
 R. P. Marshall* H5-61
 G. A. Meyer* S2-48
 R. J. Murkowski* H5-03
 R. M. Orme H5-27 *Orme*
 R. D. Powell G3-21
 73510 File/LB H5-27
 * w/o Attachment

This memo transmits the "TWRS Privatization Process Technical Baseline Assumptions and Bases." These Assumptions and Bases are a predecessor to the TWRS Privatization Process Technical Baseline document that will be completed later this year. The Process Technical Baseline, a summary level flowsheet of privatized tank waste processing, will complete High-Level Waste Program milestone T33-96-204 and Low-Level Waste Program milestone T32-96-018. Both are DOE-RL milestones.

A draft of these Assumptions and Bases circulated for comment in January, 1996 (Milestone Control No. T32-96-019). The comments resulted in substantial revisions to the draft. Material from several recently issued studies was also included in these revised and improved assumptions. We are now ready to proceed with preparation of the Process Technical Baseline document.

Further questions or comments on the Attachment should be directed to R. M. Orme (372-0035).

D. J. Washenfelder

D. J. Washenfelder
 Manager

Attachment

TWRS PRIVATIZATION PROCESS TECHNICAL BASELINE
ASSUMPTIONS AND BASES

1.0 INTRODUCTION

In 1995, the United States Department of Energy (USDOE) advised its Hanford contractors to plan for the privatization of certain Tank Waste Remediation System (TWRS) functions (Bader 1995). The privatization strategy is implemented in two phases. Phase I will demonstrate the technical and business viability of using privatized facilities to pretreat and immobilize a limited amount of Hanford tank waste, the treated products returning to USDOE for interim storage and disposal. Phase II shifts more of the TWRS functions (retrieval, in-process storage, sludge pretreatment) into the private sector and builds full-scale treatment facilities to process the balance of the waste.

Responding to the privatization strategy, the Waste Disposal Program identified the need for a *TWRS Privatization Process Technical Baseline (PTB)* (Milestone T32-96-018) to support the Systems Engineering of privatized Hanford waste processing. The intent and scope of the *PTB* task as defined in the Schedule Activity Planning Form is as follows:

"Revise the TWRS Process Flowsheet¹ to a summary level technical baseline document. The work will provide the technical bases for privatization to support systems engineering analysis, and will provide an ASPEN model that can be used to support retrieval sequence and blending work. The work will only be performed in sufficient detail to identify M&O contractor and private vendor interfaces and support the retrieval sequence work."

The purpose of this letter is to assemble under one cover the *Assumptions and Bases* for preparation of the *PTB*.

Our original intention was to produce a TWRS Process Flowsheet-like document. On 1/15/96 we circulated draft *Assumptions and Bases* (Milestone Control Number T32-96-019) to disposal program managers for discussion and comment. Considering that the *TWRS Privatization Request for Proposals (RFP)* (DOE 1996) does not obligate private contractors to select previously favored processes, reviewers felt that the Phase I *PTB* should reflect a level of detail commensurate with the direction found in the *RFP*.

The *RFP*, in fact, is silent on separations and immobilization process technology. Even vitrification, the "selected" architecture for high-level waste (HLW) immobilization (DOE 1990), is not fixed because the *RFP* allows private contractors to propose alternate waste forms. The privatized process envelope is a "black box" producing waste packages that are defined by the *RFP* in terms of their physical characteristics, minimum waste loading, and maximum

¹The *TWRS Process Flowsheet* (Orme 1994, 1995) mentioned above has been the Systems Engineering model for projecting the volume of major products resulting from the processing of tank waste.

radionuclides. The volume of secondary waste streams is dependent on process selections yet to be made by the private contractors.

Arriving at *Assumptions and Bases* for Phase I is complicated by the flexibility of the private procurement. There will be two private contractors, each of which can exercise a choice of two options. The low-level/high-level option requires private contractors to receive two waste feed streams and return two product streams. The low-level only option requires the receipt of one waste feed stream, and the return of one product stream and three or four intermediate product streams.

Unfortunately, Bader (1995) provides only general guidance for Phase II, and the *RFP* does not address Phase II at all. We know only the schedule and that Phase II entails low-level and high-level processing of the balance of the waste. Pending further guidance on Phase II, the *ASPEN PLUS TWRS Process Flowsheet* (Orme 1995a) model, brought up to date with adjusted feed streams and latest process chemistry data, is a reasonable basis for projecting Phase II processing results. There are, incidentally, no plans to issue a second revision of the *TWRS Process Flowsheet* document. Phase II modeling with the *TWRS Process Flowsheet* model will be reflected in Rev. 0 of the *PTB* document.

Phase I Part A is a 20 month period, targeted to end April 30, 1998, for contractors to prepare deliverables, and for USDOE to evaluate and select contractors for Part B. The deliverables include a schedule, the equivalent of a conceptual design report, a product qualification plan, a regulatory compliance plan, etc. Phase I Part B allows four years to design and construct, five years for operations, and one year for deactivation. USDOE may exercise options to extend the duration of operations. Some of the key schedule targets (DOE 1996) for Phase I are as follows:

Award none, one, or more Part A design only contracts	September 1, 1996
Complete contractor evaluation and authorize Part B	April 30, 1998
Begin proof-of-concept operations	June 1, 2002

Some of the key schedule targets (Bader 1995) for Phase II are as follows:

Award contract	2005
Begin LAW operations	2011
Begin HLW operations	2013
Complete processing of LAW	2021
Complete processing of HLW	2028

As a final note, Systems Engineering is the USDOE-approved approach for selecting and acquiring the waste disposal architecture of TWRS. While Systems Engineering functions and requirements decomposition and supporting documentation for waste processing has progressed to the 4th level (WHC 1996), there are as yet no official decisions (wash sludges vs. dissolve sludges, minimum radionuclide separations vs. extensive radionuclide separations, vitrification vs. some other treatment of LLW) on processing architecture with the exception of HLW vitrification.² It appears that USDOE is using privatization, not only as a contracting strategy, but as a vehicle for expediting architecture decisions under the Systems Engineering umbrella.

²As noted above, with the procurement of privatized services, even the vitrification of HLW is open to alternative architectures.

2.0 OBJECTIVES

We identify under this cover the major flowsheeting *Assumptions and Bases* that will govern preparation of the *TWRS Privatization Process Technical Baseline*. The baseline encompasses two flowsheets. The Phase I flowsheet is a high-level flowsheet that projects the volume of major, intermediate and secondary product streams for the *RFP*-defined scenario without resorting to selection of specific technology. The Phase II flowsheet, which processes all the waste left over from Phase I, is a high-level summary of the *TWRS Process Flowsheet*.

To date, the customers of the *PTB* task have expressed a variety of expectations. The process flowsheet format is suitable for meeting some expectations but others are better met by supplemental work such as tank sequence modeling.³ The author understands the primary expectations to be:

- (1) provide a model for projecting the outcome of privatized TWRS processing,
- (2) describe and quantify under one cover the interfaces between the Phase I privatized process envelope and USDOE operations, and
- (3) continue support of the M-50-03 annual enhanced sludge washing status report, i.e., project waste volumes to the end of processing using currently available information.

We cannot carry the *PTB* to the same level of detail as our previous flowsheeting efforts because detailed process work is the scope of private contractors; the *PTB* is not a project definition or process design document. Architecture selections may not be known until the private contractors submit their Part A deliverables in December 1997. In the meantime (about one and a half years), we will maintain a *PTB* at a level of detail that is commensurate with the available procurement guidance.⁴ We expect that the *PTB* will become more detailed as TWRS Systems Engineering matures in the newly privatized environment.

³For example, our flowsheet format can project total material flow for the two phases of privatization. Minimum processing rates could be inferred from the *RFP*, but process design (equipment design and equipment sizing) falls within the scope of the private contractor.

⁴Historically, *TWRS Process Flowsheet* work has proceeded in a somewhat similar environment. We have had to anticipate the results of Systems Engineering studies and decision boards by making tentative architecture selections.

3.0 ASSUMPTIONS AND BASES FOR THE PRIVATIZATION PROCESS TECHNICAL BASELINE

TWRS Technical Integration recently revised the *Functions and Requirements* (WHC 1996) for the Process Waste function to reflect the new requirements of privatization (Bader 1995). The companion *Baseline System Description* (Johnson 1996) indicates that the private contractor will evaluate and select suitable architectures for pretreating supernatants and immobilizing LAW, although it should be noted that the January 1996 draft amendment to the *Hanford Facility Agreement and Consent Order (Tri-Party Agreement or TPA)* still assumes that Hanford will produce a vitrified ILAW.

Key sources either completed or in progress provide DST consolidation recommendations (Powell et al. 1996)⁵, privatization HLW staging plans (Manuel et al. 1996), privatization LLW staging plans (Certa et al. 1996), and overall tank retrieval sequence recommendations (Penwell et al. 1996). The author of the *PTB* intends to draw upon these sources when appropriate for establishing the technical baseline feed materials.⁶ The primary vehicle for communicating requirements to private contractors is the *TWRS Privatization Request for Proposals (RFP)* (DOE 1996). The *Assumptions and Bases* are derived to a large extent from these sources.

New technical reports addressing important aspects of the process such as settling and thickening of settled sludge are also available. The body of empirical enhanced sludge washing efficiency data grew considerably during 1995, and will continue to expand during 1996. The results of a LLW melter test program are also available. In short, there is a wealth of new information for revising and improving the old technical baseline.

TWRS process knowledge is, to a large extent, empirical. The status of tank waste characterization, the complexity of the chemistry, and the status of commercially available software precludes a rigorous thermodynamic approach to chemical process modeling. The assumptions pertaining to mass balance calculations assembled for this letter are derived from a mixture of laboratory data, engineering approximations, experience, and some intuitive judgement. Improving the flowsheet's calculational methods is a standing objective; readers of this *Assumptions and Bases* letter and the subsequent *PTB* are encouraged to challenge assumptions and suggest improvements or alternative methods.

A draft of renegotiated TPA milestones is currently circulating for public comment and should be finalized by April 1996. Major TPA milestones for retrieval (the M-45-00 series) remain in effect for privatization, but interim milestones will probably be renegotiated. Sludge immobilization

⁵The current status of the consolidation decision is that DSTs will not be consolidated.

⁶ Much of the key information in these studies was recently extracted and summarized in the TWRS Disposal Program's periodic submittal of assumptions to the Operational Waste Volume Projection (Honeyman 1996).

milestones (the M-51-00 series) will be met by privatization plans, assuming that at least one of the private vendors exercises the HLW vitrification option during Phase I. USDOE is still obligated to begin HLW vitrification by December, 2009 if Phase I vendors do not pursue the HLW option. The main effect of renegotiation is the deletion of a number of LLW pretreatment milestones (the M-50-00 series), which reappear in the M-60-00 series as privatized LAW pretreatment and immobilization milestones. The sludge pretreatment milestones of the M-50-00 series are still in effect.⁷

3.1 KEY ASSUMPTIONS FOR PHASE I

The M&O contractor's role during Phase I is to provide access to process water, potable water and electricity, to prepare and transfer a limited amount of sludges to HLW immobilization, to provide LLW feeds to the private contractors, and to receive back finished products and intermediate products for storage and disposal. The M&O also receives back secondary wastes that cannot be dispatched through private channels.

Certain private contractor interfaces are excluded from consideration in the *PTB* because they are either extraneous to the waste disposal process, or because the interface is not with USDOE. Private contractors must, for example, make their own arrangements for non-radioactive/dangerous solid wastes, non-radioactive/non-dangerous solid wastes, and liquid sanitary wastes. Land, deactivated facility and site, roads and rails, and non-routine HLW have no material effect on the process mass balance.

Figures 1 and 2 depict the M&O/private contractor interfaces for the two contract options: LAW-only processing and LAW/HLW processing. The *PTB* will track only those interfaces that are pertinent to projecting the volume of products and routine secondary wastes received by the M&O. Phase I products are defined in general terms because private contractors have yet to select their waste treatment architecture.

3.1.1 Characterization

- The Characterization Project's standard inventory task is a work in progress. A best-basis (i.e., standardized tank-by-tank inventory) will not be available to support process baselining.

⁷TPA milestone dates generally are later than those reflected in the official planning documentation. The Washington State Department of Ecology, a cosigner of the *Hanford Facility Agreement and Consent Order (Tri-Party Agreement or TPA)* fully supports efforts to complete commitments ahead of the TPA schedule. The *Assumptions and Bases* document is being prepared concurrent with the public comment period for the renegotiated TPA milestones. Consequently, there may be discrepancies between this *Assumptions and Bases* document and the final version of TPA.

Figure 1 LAW Only Processing
 Important Interfaces

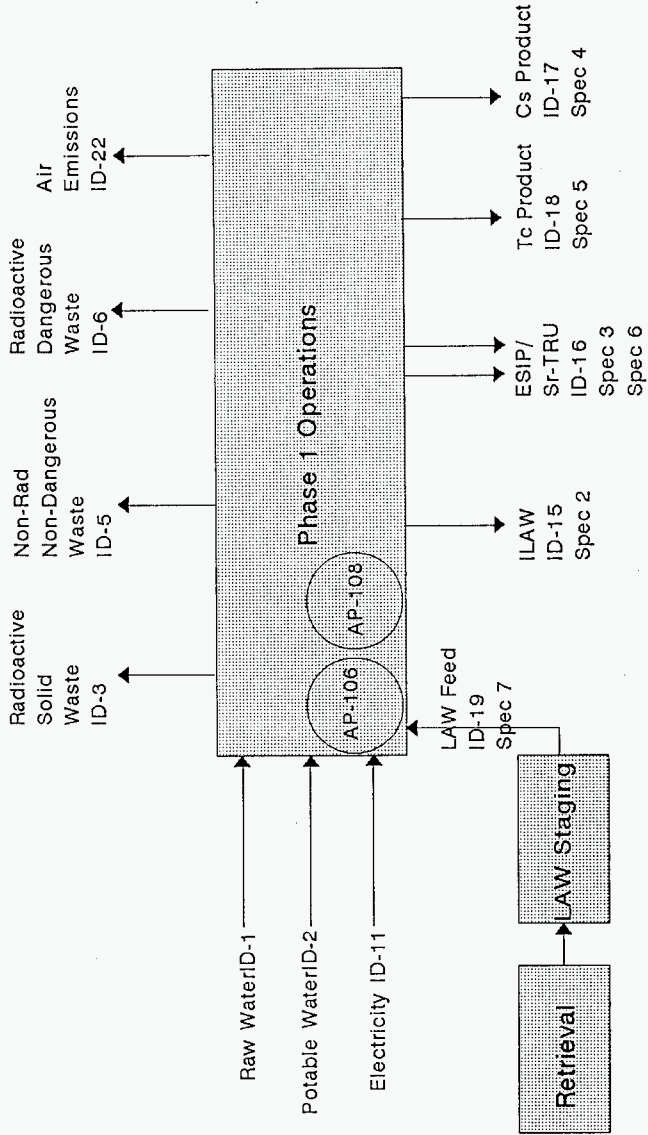
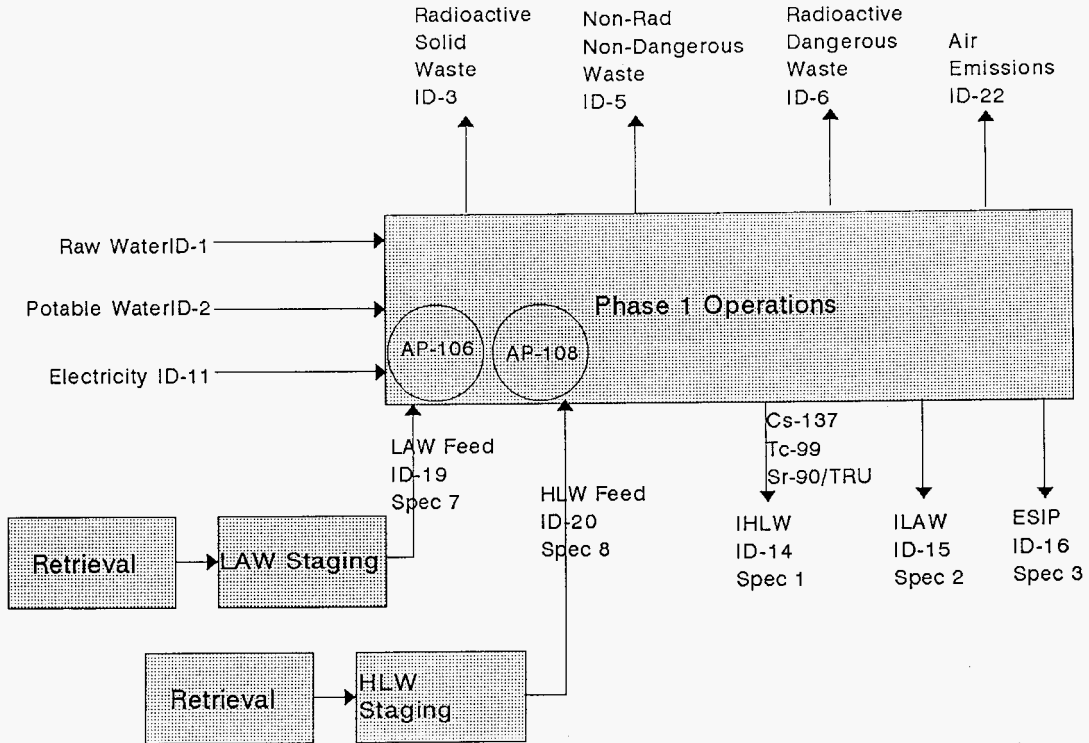


Figure 2 LAW/HLW Processing Important Interfaces



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 TMS PRIVATIZATION PROCESS TECHNICAL BASELINE

- Phase I feeds are consistent with the feeds as defined in preliminary feed staging plans (Certa et al. 1996 and Manuel et al. 1996). If subsequent revisions of the staging plans become available in time, that information will be included.
- The location of waste is consistent with TWRS Disposal Program's latest waste transfer input to the periodic Operational Waste Volume Projection (Honeyman 1996). Supernate composition and inventory are consistent with Shelton (1996).
- Private contractor intermediate waste returns added to one of three global inventories minus the feed to Phase I constitutes the feed to Phase II. (See Section 3.2.1 for the details pertaining to Phase II feed).

3.1.2 Retrieve Waste

- The M&O contractor will retrieve the full minimum amount of Envelope A, B, and C in turn into intermediate feed staging tanks before providing additional orders. The combined amount of Envelope A, B, and C will not exceed 5,100 MT of sodium per contractor, and we assume that each contractor processes the maximum amount of feed. The range of feed from each envelope is as follows:

Envelope A	2,600-4,900 MT of waste sodium
Envelope B	100-1,000 MT of waste sodium
Envelope C	100-2,400 MT of waste sodium

- The amount of envelope D may range from 245-465 MT of waste oxides per contractor excluding sodium and silicon. The flowsheet will process the retrievable amount of DST sludge identified by Manuel et al. 1996, but that may be insufficient to reach the maximum.
- DST liquids and solids for Phase I will be retrieved to the extent shown in the feed staging plans. Solids will be transferred with mixer pump/transfer pump systems.

The total feed to Phase 1 based on the feed staging plans is summarized in Attachment 1.

3.1.3 Transfer Waste

- Waste transfers are within the existing and future underground piping system.
- During retrieval and transfer, highly concentrated liquors are diluted to 1.4 spg, the maximum spg allowed without evoking a gas accumulation analysis.
- The PTB will evaluate the potential for solids precipitation during the dilution of concentrated liquors.

3.1.4 Store In-Process Waste

- AP-102 and AP-104 are set aside for the tank farm operator to prepare and stage retrieved liquids to the private contractors tanks.
- LAW feed is provided to AP-106 and A-108 which have been designated as the Contractor waste feed tanks. The M&O will transfer no more than 5 vol% solids to these feeds.
- HLW feed exists in AZ-101 (available in May 1998), AZ-102 (available in May 2001) and AY-102 (combined AY-102 and C-106 solids, available in June 2004) as defined in Honeyman (1996). HLW feed is provided by pipeline to a point of connection in the vicinity of the AP tank farm, but received and stored in Contractor provided facilities.
- A fifth AP tank is set aside for receiving the Entrained Solids intermediate product from the contractors. We assume that the contractors consolidate TRU/Sr intermediate product, if there is one, with Entrained Solids.
- Private contractors are not required to provide evaporator capability for managing waste volume. Therefore, the M&O contractor will extend operations of 242-A to at least 2011 to manage waste volume and, if necessary, control the concentration of feed to private contractors. (The previous TWRS baseline provided evaporation through the pretreatment facility beginning in 2004).

3.1.5 Pretreat LAW

- The transfer schedule for supernatants to the contractor is in Honeyman (1996), unless superseded by the revision of Certa et al. (1996).
- The RFP-defined separations on LAW feeds result in Entrained Solids, Sr-TRU, Tc, and Cs intermediate product streams. It is a contractor responsibility to evaluate and select the separations technology. At this point in time, we can only say that the intermediate product streams are within the specifications defined by the RFP.

Specification 10 limits the impact that intermediate product streams may have on IHLW by placing ceilings on the amount of total oxide equivalents in all of the intermediate product streams and the amount of sodium in specific intermediate product streams.

- Per metric ton of Na in the LAW feed, contractors may add no more than 100 grams in total of the following: fluorine and chlorine, and the oxide equivalent of sulfur, phosphorus and chromium.

- Given that the total Na in LAW feed is 10,200 MT, Specification 10 allows private contractors to add/precipitate no more than 102 MT of oxide equivalent (excluding Si and Na) in the four intermediate waste products.

3.1.5.1 Entrained Solids Intermediate Product (ESIP)

The contractors are allowed to return Entrained Solids Intermediate Product, and we assume that they return this stream. Entrained Solids has reference to the carrier liquid and solid particles, i.e., the slurry returned by the Contractor. An LAW-only contractor is allowed to combine Entrained Solids with the Strontium and Transuranics product, and we assume that this is done.

Entrained Solids has the potential to be a large volume stream if the M&O contractor takes advantage of the 5 vol% solids⁸ allowed in the feed stream. With Entrained Solids required to be 20-30 vol% solids, Entrained Solids volume could be as high as 25% of the LAW feed to the contractor. We expect that the LAW will contain much less than the 5 vol% solids that is allowed.

- Entrained Solids contain no more than 5% of the Cs-137 in the LAW feed (Specification 3).
- Entrained Solids contain no more than 5% of the Tc-99 in the LAW feed (Specification 3).
- Entrained Solids contain no more than 60 grams Na per kg of insoluble solids (Specification 10).

3.1.5.2 Strontium and Transuranic Intermediate Product (STIP)

LAW-only contractors are allowed to return a strontium and transuranic intermediate product which may be mixed with Entrained Solids. We assume that contractors combine STIP with ESIP and the assumptions are the same as for the Entrained Solids (Specification 6).

3.1.5.3 Technetium Intermediate Product (TIP)

LAW-only contractors are allowed to return a Tc intermediate product stream. TIP is returned as a solution or slurry. TIP is not returned to USD OE until the end of Phase I processing.

- TIP contains no more than 0.0015 Ci per liter of gamma emitting radionuclides with energies greater than 0.4 MeV (Specification 5).

⁸In the context of this RFP and this TPB, vol% is understood to be the settled volume fraction, not the liquid displacement.

- TIP contains no more than 10 kg Na per metric ton of Na in the LAW feed. Since LAW-only contractors process 10,200 MT of Na, TIP may contain up to 102 MT Na (Specification 10).

3.1.5.4 Cesium Intermediate Product (CIP)

LAW-only contractors are required to return a Cs intermediate product stream. Cs intermediate product is a right circular cylinder with external dimensions 33 cm in diameter and 137 cm high containing a dry, free flowing material.

- CIP contains no more than 1% of the Tc-99 in the LAW feed (Specification 4).
- The radiolytic heat of any container cannot exceed 1.5 kW (Specification 4).
- CIP contains no more than 10 kg Na per metric ton of Na in the LAW feed. Since LAW-only contractors process 10,200 MT of Na, CIP may contain up to 102 MT Na (Specification 10).

3.1.5.5 Pretreated LAW

- The amount of Sr-90, Tc-99, and Cs-137 (see Section 3.1.6) allowed in ILAW is assumed to satisfy NRC's requirement to remove key radionuclides to the maximum extent that is technically and economically practical.
- The pretreated waste is capable of being incorporated in a solid physical form at a concentration that does not exceed the applicable concentration limits for Class C LLW as set out in 10 CFR 61.

3.1.6 Immobilize LAW

A Systems Engineering study (Higley 1995) completed during 1995 evaluated the existing data on cement grouts, containerized glass, glass-in-sulfur, and polyethylene (organic binder) waste forms against systems engineering measures and the U. S. Nuclear Regulatory Commission waste form technical position. Higley's evaluation stopped short of recommending a waste form for ILAW, nor did it de-recommend the glass cullet-in-sulfur waste form that has previously been the *TWRS Process Flowsheet* baseline.

We will likewise make no assumption about the ILAW form. However, considering the *TPA's* stated preference for ILAW glass and the time line for Phase I, it's not unreasonable to assume that private contractors will opt for glass in the *RFP* specified rectangular packages.

- Direction from USDOE (Brown 1996) puts the packaged volume at 182.8 cm³ per gram mole of Envelope B sodium (7.95 m³ per MT of sodium), and 73.1 cm³ per gram mole of Envelope A/C sodium (3.18 m³ per MT sodium). The maximum volume of packaged ILAW from Phase

I allowed by the *RFP* is 250 cm³ per gram mole of Envelope B sodium, and 100 cm³ per gram mole of Envelope A or C sodium.

- The package count is flexible because the *RFP* allows +/- 0.2m to the nominal package dimensions of 1.8m x 1.2m x 1.2m standard package. The minimum size package 1.6m x 1.0m x 1.0m and the maximum size is 2.0m x 1.4m x 1.4m. The range of package volume is considerable: 1.6m³ to 3.92m³. The standard package is 2.59 m³.
- Each package of ILAW shall satisfy the criteria for classification as a Class C waste as defined in 10 CFR 61.55. (Class B or A is also acceptable). These criteria define suitability for near-surface disposal. The classification protocol allows the generator to average radionuclide concentration over the volume of the waste. The Branch Technical Position on Concentration Averaging and Encapsulation dated January 1995 clarifies that classification of solidified liquids is based on the volume or weight of the solidified mass, rather than the volume of the liquid, or the volume of the container.
- The running average concentration in ILAW (total curies divided by total ILAW volume) shall not exceed the following limits for selected radionuclides:

$$\begin{aligned} \text{Sr-90} &< 20 \text{ Ci/m}^3 \\ \text{Tc-99} &< 0.3 \text{ Ci/m}^3 \\ \text{Cs-137} &< 3 \text{ Ci/m}^3 \end{aligned}$$

- Waste constituents not immobilized in the ILAW form must be accounted for in the intermediate and secondary waste streams. The disposition of water, for example, will depend on the selection of waste form.
- Hot operations begin June, 2002 for Phase I and 2011 for Phase II.

3.1.7 LLW Disposal

- To ensure compatibility with transport, interim storage and disposal facilities, ILAW packages shall not exceed 10 MT.
- To ensure compatibility, dose rate on the external surface shall not exceed 1 Rem/hr, and surface contamination shall not exceed 367 Bq/m² for alpha and 3,670 Bq/m² for beta-gamma.
- ILAW packages will be placed in interim storage awaiting placement in a near-surface disposal facility.
- ILAW packages will be placed in an onsite near-surface disposal system that will allow retrieval for up to 50 years from the time of emplacement.

- Disposal is managed, pursuant to the Atomic Energy Act, so that safety requirements comparable to the performance objectives set out in 10 CFR 61 are satisfied. The performance of ILAW packages is a private contractor responsibility.

3.1.8 Pretreat HLW

- As a result of in-tank demonstrations and consolidation actions, ready-to-transfer water-washed solids exist in AZ-101, AZ-102 and AY-102. DOE may elect to do caustic leaching on HLW if it results in a smaller volume of IHLW for the waste form selected by the private contractor. The *PTB* will describe both the water washed and caustic leached feed to the private contractors. Based on the HLW Staging Plan (Manuel et al. 1996), caustic leaching does not reduce borosilicate glass production from Phase I because the limiting component in these solids is iron.

3.1.9 Immobilize High-Level Waste

- The transfer schedule for washed solids is in Honeyman (1996), unless superseded by a new revision of the HLW staging plan (Manuel et al. 1996).
- The *RFP* is not specific about waste form. USDOE will consider alternatives to borosilicate glass, provided the Contractor can provide adequate documentation. Consequently, the *PTB* is limited to projecting maximum IHLW volume on the basis of equivalent waste oxides in the feed.
- In the IHLW context, waste oxides has reference to the oxide equivalent of the HLW feed excluding sodium and silicon, and also excluding materials originating from LAW processing.
- The Contractor may produce no more than 1.54 m³ of IHLW per metric ton of waste oxides. This limit is equivalent to 25 wt% waste oxide loading in borosilicate glass.
- During Phase I, the HLW package count may be based on one or more of the following: Defense Waste Processing Facility canister (0.62 m³), West Valley Demonstration Project canister (0.8 m³), or a contractor proposed canister that requires USDOE approval during Part A. The Office of Civilian Radioactive Waste Management recently agreed to the technical acceptability of a 4.5m (15 ft) tall canister (1.17 m³) (Milner 1996). The parenthetical volume is the net waste volume in the package.
- Hot operations begin June, 2002 for Phase I and 2013 for Phase II. Phase I satisfies the TPA commitment to begin HLW vitrification by 2009.

3.1.10 Store High-Level Waste

- Interim storage of vitrified HLW canisters uses two vaults in the existing Canister Storage Building (Calmus 1996). Standard canisters are stacked three deep in 220 storage tubes. The CSB can handle up to 1320 standard canisters. Transfer of HLW casks to the geological repository is assumed to begin in 2035 after HLW vitrification is completed.
- Cesium intermediate product cans are likewise stored in the Canister Storage Building if the private contractors do not vitrify HLW.

3.1.11 Radioactive Solid Wastes

USDOE will accept an unspecified volume of radioactive solid wastes that comply with Hanford Site Solid Waste Acceptance Criteria (WHC-EP-0063). The volume could differ significantly between contractors depending on their process. For example, vitrification of LAW may generate a secondary waste to contain volatile Cl or F, where an alternate ILAW form may incorporate those constituents. One contractor may generate spent ion exchange resin, where the other generates no spent resin. It is the contractors' responsibility to estimate the nature and volume of waste that their respective facilities will generate.

3.1.12 Non-Radioactive, Non-Dangerous Liquid Effluents

USDOE will accept up to 300,000 m³/yr of treated effluents from each contractor for disposal at the Treated Effluent Disposal Facility (TEDF). The effluents must meet the requirements of the TEF Interface Control Document (WHC-SD-W049H-ICD-001) and the State Waste Discharge Permit. The contractors' treated effluent volume depends entirely on water usage patterns within their respective plants.

3.1.13 Radioactive, Dangerous Liquids

The volume and composition of the contractors' untreated effluent depends on the flowsheet within their respective plants. Subject to the conditions outlined below, USDOE will accept up to 100,000 m³/yr of radioactive, dangerous liquid effluents from each contractor for treatment through the Liquid Effluent Retention Facility (LERF)/Effluent Treatment Facility (ETF). LERF provides up to 50,000 m³ (13,000,000 gal) of surge capacity between the contractors and ETF. Estimating that Phase I contractors could generate a total of 10,000 to 20,000 m³/yr and assuming that liquids transferred to LERF must be treated at ETF within a year, an annual campaign at ETF appears appropriate for treating Phase I effluents.

Acceptance of waste (McDonald 1994) at ETF is contingent on three mandatory regulatory criteria. Contractors have to characterize their effluents per an approved analysis plan so the waste can be designated. ETF can accept only the waste codes listed in the Delisting Petition and the RCRA Part B Permit. The absorbed radiation dose to a hypothetical individual at

the site boundary may not exceed the dose permitted by the Radionuclide Air Emission Program (RAEP) permit.⁹

ETF may treat effluents that fall within the known envelope of treatability. ETF personnel can also identify, through the waste acceptance process, facility and/or permit modifications to prepare for accepting other wastes.

In addition to the mandatory criteria, the acceptance process for ETF considers several other factors that could affect the operability of the ETF process such as separable organics, too much dissolved organic, colloidal matter, scale forming compounds, corrosive constituents, UV absorbers, and neutral radionuclides. ETF must also satisfy certain requirements with regard to radioactive inventory in the facility and in the secondary waste product.

3.1.14 Air Emissions

For air permitting purposes, privatization contractors are integrated into the Hanford Site Air Operating Permit. To comply with the Hanford Site Air Operating Permit¹⁰, the effective dose equivalent (EDE) from all Hanford facility radionuclide air emissions must not exceed 10 mRem/yr to any member of the public during any 12-month period. Presumably, a fraction of the allowance will be allocated to the private contractors. In addition, Derived Concentration Guide-public values for individual airborne emissions shall not be exceeded at any ground-level location or occupied area as a result of Hanford operations. Best Available Radionuclide Control Technology (BARCT) and Best Available Control Technology (BACT) for toxics are required.

3.2 KEY ASSUMPTIONS FOR PHASE II

3.2.1 Characterization

For the purposes of the *PTB*, the Phase II feed consists of the total inventory plus the intermediate waste products returned from private vendors minus the DST waste transferred to private contractors during Phase I. Phase I feeds, discussed in Section 3.1.1, are based on DST tank-by-tank inventory tables that were projected to the start of Phase I (Shelton 1996 and Manuel 1996).

The total inventory in Hanford tanks is currently in transition as the Standard Inventory project works toward a final recommendation. The Characterization Project's task to develop and maintain a Standard Tank-by-Tank Inventory for all tanks will not be completed in time, and in fact is not required for the *PTB*. In the meantime, the *PTB* will present cases based on all three of the following preliminary total inventories:

⁹Permits can be modified, so being outside of permit conditions does not absolutely preclude acceptance.

¹⁰Hanford has applied for the Site Air Operating Permit, but approval is not expected until some time in 1997.

The TWRS Process Flowsheet inventory¹¹

An adjusted TWRS Process Flowsheet inventory

The LANL Rev. 3 inventory (Agnew et al. 1996)

The Standard Inventory project has arrived at "final" values for certain key waste components: Al, Cr, Fe, Na, and PO₄. These account for the "adjustment" to the TWRS Process Flowsheet inventory mentioned above. Reviews of the LANL methodology for estimating tank inventory have identified a number of flaws, and the Standard Inventory project is geared toward fixing those problems. The Standard Total Inventory and Standard Tank-by-Tank Inventory should be finalized in 1997.

3.2.2 Retrieve Waste

The details of retrieving individual tanks and tank closure is outside the scope of the *PTB*. Since privatization delays full-scale production from 2004 to 2011, privatization clearly impacts the first several years of retrieval compared to the previous retrieval baseline (Certa 1995a). The merits of alternate retrieval sequences continues to be studied (Penwell et al. 1996) in parallel with the preparation of this process flowsheet.

Table 3-1 Primary Retrieval Assumptions

Waste was conditioned at the site of retrieval or in Retrieval Annexes to facilitate long distance transfers. Conditioning may include one or more of the following: further dissolution of salts, dilution, particle size adjustment and blending. Particles should be no larger than 2 mm to be suspended at normal transport velocity.

The Phase II feed stream to pretreatment is a composite of all tank waste not immobilized during Phase I.

As a simplifying assumption for mass balance purposes, the retrieved composite feed stream shows all water soluble constituents in solution with the volume adjusted to yield a 5M Na solution. If the composite slurry is more than 10 wt% solids, additional retrieval water is added.

No additional DSTs will be provided for receiving SST waste.

- SST wastes will be retrieved starting in December 2003.¹² The maximum duration of SST retrieval is established in the language

¹¹The TWRS Process Flowsheet (Rev. 1) used a revised Hanford Defense Waste Environmental Impact Statement inventory. The revision was an increase in the amount of Al and Cr.

¹²Retrieval of SST 241-C-106 will be started in October 1996 and completed by September 2003 to demonstrate SST retrieval, and resolve the high heat safety issue.

of the Tri-Party Agreement. All SST retrieval is completed by September 2018.

- Sluicing will be acceptable as the primary SST retrieval method. Other retrieval methods may be required when there is potential for leakage or when residues are resistant to sluicing, but the method does not affect the overall mass balance.
- The process mass balance reflects 100% SST retrieval. The SST retrieval goal is 99% waste removal per the TPA so the mass balance is slightly conservative.
- SSTs are retrieved into DSTs and composited with residual DST waste to become the feed for Phase II.
- The allowable content of DSTs at the end of production has not been stipulated, but we assume the DSTs are empty for mass balance purposes.

3.2.3 Transfer Waste

The *PTB* will summarize slurry rheology data to the extent possible. Understanding the rheology of dense salt solutions and small particle (less than 40 microns) slurries is essential for pipeline operations, the assumed method of waste transfer.

Non-settling slurry rheology can be highly dependent on the nature of the particles; for example, boehmite (ALOOH) slurries are considerably more viscous than gibbsite ($Al(OH)_3$) at low shear rates. With rheology data in hand, the design of pipeline transfer systems is straightforward. Design methods for non-settling slurry pipelines are readily available (Brown and Heywood 1991).

Transfer systems for settling slurries (containing several percent solids that are greater than 50 microns) must be capable of maintaining the minimum transport velocity. The typical value is 1.8 m/sec to preclude solids deposition. Minimum transport velocities are normally correlated using solids concentration, relative densities, particle diameter, and pipe diameter. Design methods for settling slurry pipelines are likewise readily available (Durand 1953, Hughmark 1961, Spells 1955, Brown and Heywood 1991). For sluiced waste, pipeline design should consider up to 10 wt% slurry at a liquid specific gravity of 1.0 to 1.25, which corresponds to a carrier liquid ranging from very dilute to 5M $NaNO_3$ solution.

3.2.4 Store In-Process Waste

Waste retrieved in the West Area is accumulated in the SY tank farm and transferred to the A tank farm complex. Waste retrieved in the East Area is accumulated in the A tank farm complex. The A tank farm complex is also the facility for in-tank treatment of sludges. Pretreated solids are stored in the A farm awaiting transfer to the vitrification facility.

In-process waste storage requirements are driven by a number of factors: successfully matching retrieval rates and pretreatment, facility configuration decisions, and the extent to which the process areas are close coupled (or the desire to decouple process areas from each other). To keep in-process storage requirements for liquids at a minimum requires very reliable and highly coordinated operations. The private contractor may decide to work within the available DST space, or provide contingency space to reduce the risk of unscheduled downtime.

In-process storage requirements for the large volume of retrieved liquids can be minimized if pretreatment processing capacity matches or exceeds the rate of retrieval. In-process storage and in-tank treatment are overlapping functions because to a certain extent they occur at the same time in the same equipment.

3.2.5 Pretreat Waste

3.2.5.1 In-Tank Enhanced Sludge Washing

- The sludge washing function architecture is allocated to the DSTs.
- Caustic leaching, sludge washing and incidental blending of Phase II solids will be adequate to achieve an acceptable HLW volume.
- Evaluation of new laboratory results will result in revised insoluble waste estimates and caustic leaching efficiency for Phase II.

Note: the following italicized text will be revised to reflect the additional results of laboratory studies that will be available later in the year.

In-tank enhanced sludge washing includes a retrieval wash (i.e., the solubilization of some components that actually occurs during retrieval and transfer of the slurries), solid/liquid separations by settle/decant, caustic leaching of selected components (Al, PO_4^{3-} , Cr and Na are the primary targets of leaching) from the solids, and washing of the leached solids with dilute caustic.

Table 3-2 shows a summary of experimental washing and caustic leaching results that were available as of this writing (Lumetta et. al. 1993, Rapko et. al. 1995, Tener et. al. 1995). The leach efficiencies applied to the inventory of each type of SST waste yields a mass-weighted efficiency for caustic leaching.

The Al leach efficiency deserves additional explanation. During the experimental procedure, S-104 and U-110 samples (high aluminum content sludges) were treated with caustic at 100 °C and allowed to cool to near ambient temperature before analyzing the Al. Felmy's evaluation (not yet published) of these experiments in Figures 3-3 and 3-4 shows that the experimental Al concentration in room temperature samples of caustic leach solution was at the solubility limit, meaning that revised experimental

conditions could very likely improve the efficiency of Al leaching. Assuming 62% for caustic leaching of boiled REDOX wastes in place of the experimental 35%, the overall SST leach efficiency for Al in this flowsheet is 67% instead of 55%.

The Cr and PO_4 leach efficiencies are unchanged from the laboratory values. Therefore, the SST caustic leach efficiency derived from Table 3-4 for Al, Cr, and PO_4 is 67%, 60%, and 74%, respectively.

Revision 0 of the flowsheet took no credit for Na leaching. The mass weighted average for the Na_2O content in the leached sludges of 9 recent core samples (B-111, B202, BX-105, BX-107, C-103, C-108, S-104, T-107) is 11%. To obtain a residual sludge composition of 11% Na_2O for the TWRS composite feed, a 25% caustic leach efficiency is required. Therefore, a 25% caustic leaching efficiency for Na is applied to both SSTs and DSTs.

The caustic leach efficiencies for DSTs is assumed to be the same as the previous basis of 85%, 75%, and 70% for Al, Cr, and PO_4 , respectively.

Together, the assumptions for SSTs and DSTs discussed above result in overall caustic leach efficiencies of 68%, 64%, 74%, and 25% for Al, Cr, PO_4 , and Na, respectively.

The mass balance assumptions pertaining to enhanced sludge washing are summarized in Table 3-3.

Table 3-2 Mass Weighted Wash and Leach Efficiency for SSTs

This table will be revised.

	Phosphate			Chromium			Aluminum		
	Leach (% of H ₂ O insoluble)	Leach (% of Total)	Wash (% of Total)	Leach (% of H ₂ O insoluble)	Leach (% of Total)	Wash (% of Total)	Leach (% of H ₂ O insoluble)	Leach (% of Total)	Wash (% of Total)
BtPO ₄	94%	26%	72%	47%	40%	16%	58%	54%	7%
TPB	46%	36%	22%	82%	51%	37%	81%	79%	2%
REDOX	0%	0%	99%	95%	19%	80%	77%	60%	22%
REDOX ^a (bottling)	0%	0%	9%	95%	52%	45%	35%/62%	34%	4%
PUREX	0%	0%	70%	7%	7%	4%	43%	21%	51%
TOTAL	74%	26%	64%	60%	27%	55%	55%/67%	46%	17%

^aThe Al leach efficiency for REDOX boiled waste was adjusted as explained in the text. The overall efficiency changed from 55% to 67% as a result of the adjustment. Boiled REDOX waste is identified in Beard et. al. 1964.

Table 3-3 Primary Assumptions for Enhanced Sludge Washing

Flocculent Additions: Polyelectrolyte with 4 H to 1 C (this is just a placeholder until the flocculent is actually selected). Flocculent is prepared as a 10 wt% solution. Flocculent is added to slurries at 0.019 kg of flocculent per kg of dry solid. Settled solids tie up 80% of the flocculent.

1st Stage Settling: Decanted liquids entrain 0.33% of incoming solids. Settled sludge is 20 wt% solids. Al, Cr, phosphate and Na leach from solids with efficiencies of 68%, 64%, 74% and 25%, respectively. Moles of OH⁻ consumed by leaching is 1 mole/mole Al, 1 mole/mole Cr, 3 moles/mole of phosphate. Chemical addition results in an 8 wt% slurry (Stream 14) with 3M free OH⁻ and 0.01M NO₂ after leaching has gone to completion.

No further solubilization occurs after the caustic leach. Washing of the leached solids is modelled as simple dilution of the interstitial liquor.

First Wash Tank: Decanted liquids entrain 0.33% of incoming leached solids. Settled sludge is 20 wt% solids. Chemical addition results in an 8 wt% slurry (Stream 21) with 0.1M free OH⁻ and 0.01M NO₂. This addition is the first wash.

Second Wash Tank: Same as First Wash Tank (except Stream 21 is Stream 28).

Third Wash Tank: Same as First Wash Tank (except Stream 21 is Stream 51).

Fourth Wash Tank: Decanted liquids entrain no solids. Otherwise same as First Wash Tank (except Stream 21 is Stream 58).

2nd Stage Settling: Same as 1st Stage Settling.

Aqueous makeup provides 50 wt% NaOH and 50 wt% NaNO₂ for chemical additions.

The TRU content (both soluble and insoluble) of the combined supernatants (waste liquor, leachates and wash water) resulting from the in-tank enhanced sludge washing process should average <100 nCi/g and <540 nCi/g of sodium. This will ensure that the final LLW product is <100 nCi of soluble TRU/g of LLW glass, assuming all TRU in the supernatants goes to LLW glass.

The long range goal in this series of flowsheet revisions is to account for waste solubility and leach efficiency on a tank-by-tank basis using Tank Layer Model distributions, the results of sludge experiments, and the results of chemical modelling. Until the body of laboratory data is complete enough to do true tank-by-tank calculations, mass weighted averaging of the available data supplemented by engineering judgement is the next best alternative.

The Process Technical Baseline will provide for the in-tank treatment of a small volume of TRU/Sr contaminated liquids in the inventory. Adjustment of the hydroxide concentration, chemical displacement with cations (iron, strontium), chemical oxidation and heat treatment are under consideration for this selective treatment. The exact conditions for treatment will be defined at a later date.

3.2.5.2 Out-of-Tank Supernate Conditioning

The process has the capability to condition combined supernates by organic decanting, evaporation, chemical adjustment, and polishing filtration in preparation for ion exchange.

3.2.5.2.1 Organic Decanting

Production records indicate 2.6E+6 liters of non-miscible organic liquids were discharged to the tanks over the years (Bartley et al. 1996). While nowhere near that much remains in the tanks, NPH has been detected in the head space of 38 SSTs suggesting that organic phases may be present in more tanks than just C-103. The volume of organic stated below is essentially a guess since there is no basis for estimating the volume of residual organic in the tanks. There is analytical evidence that the TBP content of the organic is 70% or more, the balance being NPH or TBP degradation products.

Table 3-4 Primary Assumptions for Organic Decanting

The supernates from in-tank processing pass through a continuous gravity decanter prior to evaporation.

The separated organic phase is 75,000 L of 70% TBP/30% NPH.

The decanter removes 100% of the organic phase.

Separated organic is shipped to off-site incineration.

The potential for adverse impacts on evaporation, filtration and ion exchange is the rationale for organic decanting.

3.2.5.2.2 Evaporation

Conditioning of decanted supernates and washes includes evaporation to a standard concentration. Ion exchange feeds that have been concentrated can be treated more efficiently than a dilute feed (Kurath et. al. 1994).

Table 3-5 Primary Assumptions for Evaporator and Condenser

Filtrate is evaporated to $7M$ Na for equipment design basis. ¹³
Solids formed in the evaporator are removed by downstream polishing filter.
Condenser recovers 99% of water vapor.
Distribution coefficient (Bottoms/Condensate): $5E+6$ for Cl and NO_3 , $3.5E+5$ for TOC, and $1E+7$ for everything else (Na in condensate is adjusted to maintain the charge balance).
Bottoms are not returned to DSTs, although a routing is provided.

3.2.5.2.3 Polishing Filtration

Evaporator bottoms are filtered through a deep bed frit filter to remove entrained solids, thus preventing blinding in the ion exchange columns. When spent, the filter bed is flushed out and combines with the Cs-depleted ion exchange effluent.

Table 3-6 Polishing Filter Assumptions

Frit composition: 77% SiO_2 , 15% B_2O_3 , 6% Li_2O , 1% CaO, 1% MgO
Frit replacement: 45 kgs (100 lbs) every $3.785E+5$ L (100,000 gal)
Filter efficiency: 1% of solids pass through the filter
Filter flush: 2 wt% solids in the flush slurry

3.2.5.3 Ion Exchange

Analysis of experimental data and engineering assessments conducted during 1994 have provided an improved technical basis for modelling the ion exchange removal of Cs (Kurath et. al. 1994; Eager 1994; Johnson 1995). An empirical correlation to predict the cesium distribution (λ value) of the baseline resin over a range of concentration and temperature is now available. The λ value and a semi-empirical column breakthrough equation are used for calculating cumulative Cs losses (i.e, bed volumes to breakthrough). On

¹³ Filtrates should be concentrated to the extent permitted by their chemistry. A short evaporation study (Powell 1995) determined that evaporation to $7M$ Na is about the onset of precipitation in a variety of wastes; the chemistry of other waste may limit the extent of evaporation.

the average, 35 bed volumes are treated between elutions, ranging from 8 to 43 bed volumes depending on the type of feed.

Na and K are assumed to load on the bed in the same ratio that exists in the feed. Insufficient data is available at this point in time to define the loading behavior of other cations. Ca, Sr, Pu and Am, for example, are expected to load to some extent, but their behavior has not been tracked in column loading studies. This area needs to be addressed in future loading studies.

The column configuration consists of redundant ion exchange lines, each consisting of two columns in series. From a design standpoint, this arrangement substantially reduces pipe and valving complexity.

The parameters selected for modelling ion exchange are as follows:

Table 3-7 Assumptions for Ion Exchange Modelling

Parameter	Value
Number of Beds in Series	2
Volume of Bed	6500 L
Volume of Series	13000 L
Feed Flowrate	1 BV/hr
Number of BVs Before Regeneration ¹	Calculated from correlations Cum. Cs loss = 1 Ci/5000 moles Na
Cesium Elution	
Residual Feed Flush	2 BV Water at 2 BV/hr
Sodium Scrub ²	
Cesium Elution	6 BV 0.5M HNO ₃ at 1 BV/hr
Residual Eluent Flush	2 BV Water at 2 BV/hr
Bed Regeneration	1 BV 0.5M NaOH at 2 BV/hr 1 BV 2.0M NaOH at 2 BV/hr

¹ Resin degrades to 80% of its original capacity after 10 cycles. To account for degradation of resin capacity with time, the model regenerates the bed at 90% of the calculated number of bed volumes.

² The sodium elution step (sodium scrub) that preceded cesium elution in Revision 0 has been omitted in Revision 1. The primary benefit of the sodium scrub was to reduce the amount of sodium in the Cs eluate, the down side being increased cycle time and Cs losses to the LLW. In the current flowsheet, the Cs eluate is neutralized and returned to the DSTs prior to vitrification. The value of a sodium scrub has not been determined for these conditions. A sensitivity study may be justified to evaluate the pros and cons of a sodium scrub.

Cumulative loss of 1 Ci/m³ in 5M Na liquid effluent is a technically feasible target, thus satisfying the NRC "incidental waste" requirement (See Section 5.1.3). The total amount of cesium to near surface disposal is considerably less than the amount that has been accepted by the NRC in past negotiations. Cumulative loss is a more meaningful measure of cesium removal efficiency than percent removal (or DF) since it is consistent with the non-steady state nature of the ion exchange operation, and also reflects in unambiguous terms the curies of Cs that are permitted to break through to LLW.

The cesium removal process is based on the cation exchange resin having the properties of CS-100 formerly manufactured by Rohm and Haas. Although it is not the highest capacity resin for Cs, CS-100 has produced the most consistent results under simulated waste processing conditions of the commercially available resins tested. The cesium will be loaded on the resin at high alkaline conditions ($\text{pH} \geq 12$) from clarified supernatant at about 25 °C.

After 10 cycles (nominally 350 bed volumes) the cesium capacity of the resin has degraded to 80% of the fresh resin capacity. Spent resin will be flushed into the ion exchange effluent stream and fed to the LLW melter.

3.2.5.4 Eluate Treatment

The eluate stream, which is mostly water and nitric with some sodium nitrate and a little cesium nitrate, is evaporated and neutralized with caustic to a free hydroxide concentration of 0.1M.

Table 3-8 Eluate Treatment Assumptions

Evaporate 90% of water and 70% of nitric acid.

Condense 99% of the vapor and recycle for elution.

Neutralize bottoms 0.1M OH^- .

3.2.6 Immobilize Low-Level Waste

3.2.6.1 LLW Feed Evaporator

Table 3-9 Primary Assumptions for Evaporator

Feed is evaporated to 10M Na for equipment design basis.

Ignore solids (salts) formed in the evaporator.

Distribution coefficient: same as supernate evaporator.

Bottoms are not returned to DSTs, although routing is provided.

3.2.6.2 LLW Glass Formulation

Low-level glass optimization studies (Feng et al. 1996) tested soda-alumina-lime-boro-zirconia-iron-silicate systems (and subsets) for processability and durability. The "Phase II" vendor glass study produced six test glasses from a LLW simulant that represents the LLW fraction of SSTs. The glass selected for modeling, LRM-5412, resulted in a homogeneous melt without evidence of phase segregation. LRM-5412 contains no added zirconium or iron. Another glass, LRM-3, has better durability, but the 6% zirconia content is unattractive from a processability (melting point) and essential material standpoint. LRM-5412 falls within the typical composition ranges for

soda-lime-boro-alumina-silicate system: 15 to 25 wt% Na₂O, 0 to 12 wt% CaO, 0 to 12 wt% B₂O₃, 5 to 12 wt% Al₂O₃, and 40 to 60% SiO₂ (Wilson et. al. 1995).

Chemical additions to the LLW melter feed are made to bring the melt within the formulation constraints stated in Table 3-11. The additives are Al₂O₃, B₂O₃, CaO, and SiO₂.

Table 3-10 LLW Glass Formulation Constraints

Al ₂ O ₃	= 12 wt%
B ₂ O ₃	= 5 wt%
CaO	= 4 wt%
Na ₂ O	= 20 wt%
SiO ₂	>= 50 wt%

Time-phased process modeling (Orme 1995b) shows that occasional slugs of high Al feed should be adjusted with Na additions to hold Al₂O₃:Na₂O at the proper ratio. If the ratio is allowed to float, glass compositions fluctuate widely. This is not an issue with the composite flowsheet because there is more than enough sodium relative to aluminum.

3.2.6.3 Melter Energy

Energy in the melter is provided by combustion. The minimum energy requirement is based on the vaporization and super heating of water to 1200 °C and the melting of the major constituent oxides. The model uses 2% more energy (i.e., kerosene) than the minimum. The heat of melting for the following oxides is considered:

Table 3-11 Heat of Melting

Na ₂ O	11.4 kcal/gmole
Al ₂ O ₃	28.0
CaO	19.0
SiO ₂	2.3
B ₂ O ₃	5.8
Li ₂ O	14
MgO	18.5

The kerosene assay is 87.3% C, 12.6% H, 0.04% O, and 0.06% N. Kerosene has a heat of combustion of 11,111 kcal/kg. Oxygen for combustion is added in 10% excess.

3.2.6.4 Volatility From LLW Combustion Melter

The fractional volatility of the melt is as shown in Table 3-12. In addition to volatility, there is physical entrainment of 2% of the glass (Boltdt 1995). The composition of entrained glass is determined after volatilization.

Table 3-12 LLW Melter Volatility Assumptions

Component	% Volatile	Comment
B ₂ O ₃	25	as NaBO ₂
CdO	33	as Cd(OH) ₂
Cl	95	as HCl
Cs ₂ O	33	as CsOH
F	67	as HF
I	100	as HI
K ₂ O	(K/Na ratio same as feed)	as KOH
MoO ₃	5	as Mo(OH) ₆
Na ₂ O	1	as NaOH
NO _x	6,000 ppm noncond 20% NO	
PbO ₂	33	as Pb(OH) ₄
PO ₄	20	as H ₃ PO ₄
Ru ₂ O ₃	33	as Ru(OH) ₃
Se ₂ O ₃	33	as Se(OH) ₆
SO ₄	90 10	as SO ₂ as SO ₃
Tc ₂ O ₇	50%	as TcO ₂
TeO ₃	33	as Te(OH) ₆

3.2.6.5 ILAW Packages

Note: The following is a major change from the TWRS Process Flowsheet Rev. 1. The entire LLW culet handling operation is replaced by casting glass monoliths in the RFP specified container (Brown 1996).

Table 3-13 ILAW Package Assumptions

Each gram-mole of waste sodium generates 73.1 cm³ of ILAW package.
The standard package is 1.2 m x 1.2 m x 1.8 m (2.59 m³).

3.2.6.6 LLW Melter Offgas Treatment

Note: Modifications to these assumptions are currently under consideration. It is likely that they will change.

LLW melter offgas treatment consists of a quench tower, venturi scrubber, demister, HEPA filtration, SO₂ absorption, and catalytic reduction of NO_x. Quenching is rapid cooling and condensing of a gas/vapor stream with a liquid spray. A venturi scrubber completes the particulate removal. Clean air requirements are assumed to drive SO_x and NO_x removal.

Table 3-14 LLW Melter Offgas Treatment Assumptions

Quench Tower: The quench liquid is 1.5M nitric acid. Quench flow rate is 26.54 times the water in melter offgas plus 2 times the gases in melter offgas. The gas effluent from the quench tower is saturated with quench liquid vapor at 75 °C (0.40 lbs vapor per lb of gases) and entrains 7.6 L (2 gal) of quench liquid per 1530 scfm of gas. Removes 100% of TcO₂, 95% of Hg, Cl and other solids.

Venturi/Separator: The scrub liquid is 1.5M nitric acid. Liquid flow to venturi is 1 volume per 1000 volumes of gas. The gas effluent from the venturi/separator is saturated with quench liquid vapor at 75 °C (0.4 lbs vapor per lb of gas) and entrains 7.6 L (2 gal) of quench liquid per 1530 scfm of gas. Removes 95% of Hg, Cl and other solids.

Demister: Removes 95% of Hg, 98% of solids. The gas effluent is saturated at 30 °C (0.0265 lbs vapor per lb of gas), with no entrainment of liquid. Demister wash is set to zero.

Scrub Solution Tank: Maintain at 1.5M nitric acid. TcO₂ converts to TcO₄⁻.

CuO Bed: Removes 90% of SO₂. Maintain 10% excess O₂ in reactor feed. Reactor chemistry is SO₂+O₂+CuO => CuSO₄. Cu/S mole ratio is 2.0 at full loading.

NO_x Reactor: Reduces ~99% of NO_x. Maintain 10% excess NH₃ in reactor feed. Reactor chemistry is NO+0.5O₂ => NO₂ and 3NO₂+4NH₃ => 3.5N₂+6H₂O.

Quench tower flow rate are based on ASPEN simulations. Entrainment assumptions are based on New Waste Calcining Facility design criteria (INEL). Venturi scrubber flow rate based on Perry's Handbook.

3.2.6.7 Sulfur Recovery

Sulfur recovery is completed by regenerating the CuO beds to release H₂S, partial burning of the H₂S to SO₂, and reduction to elemental sulfur in Claus Reactors.

Table 3-15 Sulfur Reduction Assumptions

CuSO₄ Bed: Removes 100% of sulfur. Feed 10% excess H₂ to CuSO₄ bed. Reaction chemistry is $\text{CuSO}_4 + 5\text{H}_2 \Rightarrow \text{H}_2\text{S} + 4\text{H}_2\text{O} + \text{Cu}$. Regenerate CuO bed with air purge.

Combustion Chamber: Add enough fuel to initiate the reaction (1 MT). One-third of H₂S is converted to SO₂. Reaction chemistry is $\text{H}_2\text{S} + 1.5\text{O}_2 \Rightarrow \text{SO}_2 + \text{H}_2\text{O}$.

Claus Reactors: Convert 90% in first reactor. Convert 90% in second reactor. Reactor chemistry is $2\text{H}_2\text{S} + \text{SO}_2 \Rightarrow 3\text{S} + 2\text{H}_2\text{O}$. Gas effluent is recycled to feed SO₂ absorbers.

3.2.6.8 Sulfur Secondary Waste

Sulfur recovered from the melter offgas creates a radioactive solid waste that must be returned to DOE. The molten sulfur is poured into 55 gallon drums, allowed to cool before transfer to DOE.

3.2.6.9 Chloride Removal From Scrub Solution

Note: Modifications to these assumptions are currently under consideration. It is likely that they will change.

Table 3-16 Chloride Removal Assumptions

Acid Evaporator Feed Tank (TK-1100): 25% of the recycled scrubber solution is diverted to chloride removal. No acid added (feed should already be 1.5 M HNO_3).

Acid Evaporator (EV-1102): Condensate carries 83% of water, 25% of HCl , 74% of HF , 18% of HNO_3 . Distribution coefficient for everything else is 10^7 .

Acid Distillation Column (T-1106): Overheads carry 92% of water, 99.9% of HCl , 99.9% of HF , 0.035% HNO_3 . Nothing else in overheads.

Acid Rectifying Column (T-1107): Bottoms carries 10% of water, 87% of HCl , 40% of HF , 92% of HNO_3 . Nothing else in bottoms.

HCl Catch Tank (TK-1109): NaOH is added stoichiometrically to neutralize all H^+ , $\text{Ca}(\text{OH})_2$ is added at stoichiometric + 10% to precipitate F^- , $\text{Ca}(\text{OH})_2$ is added as a 10 wt% slurry.

Acid Recycle Catch/Neutralization Tank (TK-1110): $\text{Ca}(\text{OH})_2$ is add at stoichiometric + 10% to neutralize H^+ , the 10% excess precipitates F^- , $\text{Ca}(\text{OH})_2$ is added as a 10 wt% slurry.

Grout Feed Evaporator (EV-1113): Removes water to make bottoms 5 M Na , "Others" removed like other evaporators.

Condenser (EC-1114): Acts like other condensers.

Grouting Process: Grout chemicals added equal to mass flow of stream 1122, Grout chemicals are 50% Flyash and 50% Cement. All components are solidified.

3.2.7 Immobilize High-Level Waste

- The feed to the TWRS Process Flowsheet for Phase II will be the global best-basis tank estimate minus the materials processed during Phase I.
- During Phase II, the basis for the IHLW volume projection will be the TWRS Process Flowsheet, adjusted by the blending factor and/or loading factors that are considered appropriate at that time.
- Before 2013, a 15 foot tall HLW canister is approved for geologic disposal (Milner 1996). It is the sole HLW package during Phase II, having a net glass volume of 1.17 m^3 .

3.2.7.1 HLW Melter Feed Preparation

Note: Assumptions around the centrate evaporator are being reconsidered. Assumptions around the feed adjustment reactor are being reconsidered for consistency with latest feed preparation technology. They are likely to change.

Table 3-17 HLW Melter Feed Preparation Assumptions

Centrifuge: Centrate is 0.1 wt% solids. Liquid carryover in solids is 0.12 times the centrifuged solids.

Centrate Evaporator and Centrate Evaporator Condenser: Evaporate centrate to the extent that Stream 311 is a 20 wt% slurry. Distribution coefficient (Bottoms/Condensate) $5\text{E}+6$ for Cl and NO_3 , $3.5\text{E}+5$ for TOC, and $1\text{E}+7$ for everything else (Na in condensate is adjusted to maintain the charge balance)

Feed Adjustment Reactor (FAR): Oxides with lower limits in glass are added to meet the glass composition envelope in Table 3-22, while minimizing the amount of HLW glass produced. Glycolic acid (70.6 wt%) solution added in amount equal to 0.486 of the waste oxides is in excess of the requirement. FAR evaporates water so melter feed contains at least 0.376 kg of oxide equivalent per kg.

FAR Reactions: Carbonate converts to CO_2 , 50% of nitrite converts to NO, N_2O , CO_2 , and water, 90% of Hg^{++} reduced to Hg by glycolic acid.

FAR Offgas: Contains all gases. Contains 90% of all types of mercury, 98.6% of NH_3 , and 0.03% of carbonate, nitrite, nitrate, sulfate, TOC and glycolic acid plus 0.005% of all other components.

FAR Condenser: The FAR offgas passes through the condenser as follows: 100% of all gases, 50% of mercury, and 10% of everything else.

3.2.7.2 HLW Glass Formulation

HLW glass formulation for the purposes of the *PTB* follows a simple set of rules that is applied to the composite feed. This approach is not optimized. It may be possible to develop formulation rules for subsets of the composite feed that achieve higher waste loadings. Until those rules are developed, what we have available is a property/composition study that examines a composition region of single component constraints (lower and upper bounds for each of 10 components) and multiple component constraints that is assumed to produce reasonable glass quality (Hrma et al. 1994). Hrma cautions that solubility limits for Cr_2O_3 , F, P_2O_5 , noble metals and SO_3 previously determined for specific glasses may not be applicable across the tested composition region because solubility limits are composition dependent. For example, glasses that are relatively low in Ca and relatively high in Al can solubilize more phosphorus.

Table 3-18 shows the single component ranges and solubility limits used for formulating the HLW glass in the computer model. The multiple component ranges are ignored. The ranges are based on Hrma 1994.

Table 3-18 HLW Glass Formulation Ranges (CVS@1150 °C)

Component	Glass	
	Lower	Upper
Single-Component Ranges ^a		
Al_2O_3	0.0%	15.0%
B_2O_3	5.0%	20.0%
CaO	0.0%	10.0%
Fe_2O_3	2.0%	15.0%
Li_2O	1.0%	7.0%
MgO	0.0%	8.0%
Na_2O^b	5.0%	20.0%
SiO_2	42.0%	57.0%
ZrO_2	0.0%	13.0%
Multi-Component Ranges ^c		
$Al_2O_3+ZrO_2$	≤16.0%	
$Al_2O_3+ZrO_2+Fe_2O_3$	≤21.0%	
$MgO+CaO$	≤24.0%	
Solubility Limits		
Cr_2O_3	≤0.5%	
F	≤1.7%	
$P_2O_5^d$	≤3.0%	
$Rh_2O_3+Ru_2O_3+RuO_3$	≤0.25%	
SO_3	≤0.5%	

^aThe sum of all components not listed may range from 1% to 10%.

^bIncludes K_2O .

^cAttempts to eliminate formulations with poor processability by the application of multiple component constraints have been "only partially successful" per Hrma 1994. Multi-component constraints are ignored in the model.

^dThis limit differs from the 1% ceiling used for HWVP formulations as shown in Hrma 1994. It is an engineering judgment that TWRS composite glass can solubilize up to 3% P_2O_5 .

Use of the above formulation rules generally produces less glass than the previously used HWVP formulation rules (Orme 1995a). A preliminary study of Phase I feeds comparing CVS rules and HWVP rules shows that the waste loading is still reasonable even though the glass volume is smaller (Manuel et al. 1996).

3.2.7.3 Volatility From HLW Melter

Physical conditions and chemistry in the HLW melter are quite different from the LLW melter. Volatilization occurs in the cold cap, but the cold cap also functions as a barrier to physical entrainment. All components except Al and PO_4 and those noted in Table 3-19 are completely oxidized and remain in the glass. Some gases volatilized from $NO_{x(aq)}$ undergo further gas phase reactions.

Table 3-19 High Level Melter Volatility Assumptions

Component	% Volatile	Comment
B_2O_3	1.0%	
CdO	14%	
Co_2O_3	0.33%	
Cl	0.1% 50% of balance	as Cl_2 as solid Cl
Cs_2O	7.1%	
F	0.1% 25% of balance	as F_2 as solid F
K_2O	0.33%	
MoO_3	1.0%	
Na_2O	0.33%	
NO_x	100%	75% as NO and O_2 92% of remainder as N_2 and O_2 100% of remainder as NH_3 and O_2 ¹
PbO_2	10%	
Ru_2O_3	2.5%	
SeO_3	10%	
TcO_4	50% 7.1%	as TcO_2 as Tc_2O_7
TeO_3	10%	

¹20% of NH_3 reduces to NO and H_2O ; 75% of remainder to N_2 and H_2O .

3.2.7.4 HLW Melter Offgas Treatment

Note: Assumptions around the scrubbing section are being reconsidered and are likely to change. Assumptions around mercury removal and ammonia destruction are being reconsidered and are likely to change.

Table 3-20 HLW Melter Offgas Treatment Assumptions

Quench Tower: The quench liquid is water. Quench flow rate is 26.54 times the water in the melter offgas plus two times the gases in the melter offgas. The gas effluent is saturated with water at 75 °C (0.40 lbs vapor per lb of gas) and entrains 7.6 L (2 gal) of quench liquid per 1530 scfm of gas. Removes 100% of TcO_2 , 95% of Hg, 95% of water, 95% of all solids. Solubility of NO in quench water is 1%; of SO_2 is 20%. No acid additions to quench water.

Venturi/Separator: Removes 100% of Hg, 95% of water, 50% of NH_3 , 95% of all solids.

Demister: Removes 85% of water, 98% of solids.

Scrub Solution Tank: TcO_2 converts to TcO_4^- .

Mercury Recovery: Knockout chiller removes 90% of Hg from FAR condenser vent.

Ammonia Destruction Tank: Inoperative

Condenser Vent Gas Scrubber: Removes 95% of NH_3 and 90% of Hg and other non-gaseous compounds.

Secondary Waste Evaporator: 100% of spent MOG scrub feeds the evaporator. Boils off 75% of water, 75% of NH_3 , 5 % of NO_3 , NO_2 , SO_3 , CO_3 , and TOC and 0.2% of everything else. No water or chemical additions.

Salt Waste Adjustment Tank: Inoperative. Salt waste recycled to HLW receiving vault (Tk-300 A,B,C,D,E,F).

3.2.7.5 HLW Package

Tentative acceptance of a 15 ft canister was obtained from RW (Milner 1996). The net glass volume of $1.17 m^3$ is assumed. The mechanical operations of canister closure, decontamination, smear testing, etc. are not depicted in this flowsheet.

References

- Agnew 1994a, Estimating Chemical Inventories for Hanford Tank Wastes, LA-UR-94-273, Los Alamos National Laboratory, Los Alamos, New Mexico.
- Agnew 1994b, Hanford Defined Wastes: Chemical and Radionuclide Compositions, LA-UR-94-2657, August 1994.
- Agnew et. al. 1995, Tank Layer Model (TLM) for Northwest, Southwest, and Northeast Quadrants, LA-UR-94-4269.
- Agnew et al. 1996, Hanford Tank Chemical and Radionuclide Inventories: HDW Model Rev. 0, draft, March 1996.
- Alumkal 1994a, Internal Memo, Tank Waste Remediation Technical Strategy, March 18, 1994.
- Alumkal 1994b, Alumkal to Sheridan (Letter 9454691), Configuration Selection for the Tank Waste Remediation System, July 18, 1994.
- Bader 1995, Tank Waste Remediation System (TWRS) Guidance for Update of the Multi-Year Program Plan (MYPP) -- Supplemental Guidance for the Disposal Strategy, (95-PRI-073), July 1995.
- Bartley et al. 1996, Tank 241-C-103 Systems Engineering Study: Separable Phase Skimming, Storage, Treatment and Disposal Options, WHC-SD-WM-ES-384, May 1996.
- Beard et. al. 1964, Waste Management Program Chemical Processing Department, HW-81481, 1964.
- Boldt, A. L., K. D. Boomer and E. J. Slaathaug 1995, Determination of Low-Activity Waste Fraction From Hanford Site Tanks, WHC-SD-WM-TI-699 Draft Rev. A, November 1995.
- Boldt 1995, Personal Communication, 1/31/95.
- Boomer et. al. 1993, Tank Waste Technical Options Report, WHC-EP-0616, March 1993.
- Boomer et. al. 1994, Tank Waste Remediation System Facility Configuration Study, WHC-SD-WM-ES-295, Rev.0.
- Brevik 1995a, Historical Tank Content Estimate for the Southwest Quadrant of the Hanford 200 West Area, WHC-SD-WM-ER-352, March 1995.
- Brevik et al 1995, Historical Tank Content Estimate for the Northwest Quadrant of the Hanford 200 West Area, WHC-SD-WM-ER-351, March 1995.
- Brevik 1995b, Historical Tank Content Estimate for the Northeast Quadrant of the Hanford 200 East Area, WHC-SD-ER-349, March 1995.

- Brown 1996, LLW Product Loading Assumptions for the TWRS Flowsheet, DSI from N. R. Brown to R. M. Orme, April 23, 1996.
- Brown and Heywood 1991, Slurry Handling Design of Solid-Liquid Systems, Elsevier Applied Science, 1991.
- Calmus 1996, Solidified High-Level Waste Interim Storage Alternative Analysis and Path Forward Recommendation, WHC-SD-WM-SP-011 Rev. 0, May 1996.
- Certa 1995a, Select Retrieval Sequence and Blending Strategy Decision Analysis Frame, WHC-SD-WM-RPT-107, March 1995.
- Certa 1995b, Preliminary Retrieval Sequence and Blending Strategy, WHC-SD-WM-RPT-167 Rev. 0, August 1995.
- Certa et al. 1996, Preliminary Low-Level Waste Feed Staging Plan, WHC-SD-WM-RPT-210, February 1996.
- Colton et. al. 1995, Pretreatment Chemistry Evaluation: A Status Report, TWRSPP-95-024, June 30, 1995.
- Colton 1995, Sludge Pretreatment Chemistry Evaluation: Enhanced Sludge Washing Separation Factors, PNL-10512, March 1995.
- Croft 1980a, ORIGEN2 - A Revised and Updated Version of the Oak Ridge Isotope Generation and Depletion Code, ORNL-5621.
- Croft 1980b, A User's Manual for the ORIGEN2 Computer Code, ORNL/TM7175.
- DOE 1987, Final Environmental Impact Statement, Disposal of Hanford High-Level Waste, Transuranic and Tank Waste, DOE/EIS-0113.
- DOE 1990, Evaluation and Selection of Borosilicate Glass as the Waste Form for Hanford High-Level Radioactive Waste, DOE/RL-90-27 Rev. 1, September 1990.
- DOE 1991, Integrated Data Base for 1991: U. S. Spent Fuel and Radioactive Waste Inventories, Projections, and Characterization, DOE/RQ-0006, Rev. 7.
- DOE 1996, TWRS Privatization Request for Proposals, DE-RP06-96RL13308, United States Department of Energy, Richland, Washington.
- DOE-OCRWM 1993, Waste Acceptance System Requirements Document, Rev. 0, DOE/RW-0351P, Office of Civilian Radioactive Waste Management.
- DOE-WIPP 1991, Waste Acceptance Criteria for the Waste Isolation Pilot Plant, WIPP/DOE-069, Rev. 4, 1991.
- Durand 1953, Proceedings of the Minnesota International Hydraulics Convention, September, 1953, Part I, pg. 89-103.

- Eager 1994, Preliminary Flowsheet: Ion Exchange Process for the Separation of Cesium From Hanford Tank Waste Using Duolite CS-100 Resin, WHC-SD-WM-TI-667, Rev. 0, December 1994.
- Ecology et. al. 1994, Hanford Facility Agreement and Consent Order, Fourth Amendment, January 1994.
- Felmy et. al. 1994, The Solubility of $\text{Cr}(\text{OH})_3(\text{am})$ in Concentrated NaOH and NaOH- NaNO_3 Solutions, PNL-SA-24027, August 1994.
- Feng et al. 1996, Glass Optimization for Vitrification of Hanford Site Low-Level Tank Waste, PNNL-10918, March 1996.
- Gumprecht 1968, Mathematical Basis for Computer Code, DUN-4136, June 1968.
- Hanlon 1993, Tank Farm Surveillance and Waste Status Summary Report for October 1993, WHC-EP-0182-67.
- Higley 1995, Evaluation of Low-Level Waste Forms for Immobilization of Hanford Site Tank Wastes, WHC-SD-WM-ES-319, Rev. 0, June 1995.
- Hill et. al. 1995, The Sort on Radioactive Waste Type Model: A Method to Sort Single-Shell Tanks into Characteristic Groups, PNL-9814 Rev. 2, March 1995.
- Honeyman 1996, Submittal of the TWRS Disposal Program Assumptions for the Operational Waste Volume Projection, DPO-96-14, March 1, 1996.
- Hrma et al. 1994, Property/Composition Relationships for Hanford High-Level Waste Glasses Melting at 1150 °C, PNL-10359, December 1994.
- Gasper 1995, Gasper to Sanders, Letter 9501609B R1, PROJECT W-236B TANK WASTE REMEDIATION SYSTEM (TWRS) WASTE PRETREATMENT FACILITY PRELIMINARY DESIGN REQUIREMENTS DOCUMENT, May 15, 1995.
- Hughmark 1961, Aqueous Transport of Settling Slurries, Industrial and Engineering Chemistry, Vol. 53, May 1961.
- INEL, Final Design Criteria for the New Waste Calcining Facility (NWCF), Allied Chemical Corporation, Idaho Falls, Idaho.
- Johnson 1995, Recommended Cesium Ion Exchange Process Modelling Parameters for Inclusion in the Revised TWRS Process Flowsheet, Internal Memo, M. E. Johnson to D. J. Washenfelder, March 14, 1995.
- Johnson 1996, Tank Waste Remediation System Baseline System Description, WHC-EP-0856 Rev. 1, March 1996.
- Jungfleisch 1984, TRAC: A Preliminary Estimation of the Waste Inventories in Hanford Tanks through 1980, WHC-SD-WM-TI-057, Rockwell Hanford Operations, Richland, Washington.

Kupfer et. al. 1994, WHC-SD-WM-TA-154, Strategy for Sampling Hanford Site Tank Wastes for Development of Disposal Technology, November 1994.

Kurath et. al. 1994, Experimental Data and Analysis to Support the Design of an Ion-Exchanger Process for the Treatment of Hanford Tank Waste Supernatant Liquids, PNL-10187, December 1994.

Lumetta et. al. 1993, Sludge Treatment and Extraction Technology Development: Results of FY 1993 Studies, TWRSP-93-071, September 1993.

Manuel et al. 1996, Phase I High-Level Waste Pretreatment and Feed Staging Plan, WHC-SD-WM-ES-370 Rev. 0, February 1996.

McDonald 1994, Acceptance of Feed Streams for Treatment at the LERF/ETF Complex, WHC-SD-ETF-WAC-001 Rev. 0, November 18, 1994.

Milner 1996, Evaluation of Hanford Longer High-Level Waste Product Canister Option for Acceptance by the Civilian Radioactive Waste Management System, memorandum to Jackson Kinzer, April 5, 1996.

Mitchell 1995, Immobilized Low Level Waste Disposal Options Configuration Study, WHC-SD-WM-TI-686 Rev. 0, February 1995.

Orme 1995a, TWRS Process Flowsheet, WHC-SD-WM-TI-613 Rev. 1, August 1995.

Orme 1995b, Preliminary Time-Phased TWRS Process Model Results, WHC-SD-WM-TI-693 Rev. 0, March 1995.

Penwell et al. 1996, Initial Retrieval Sequence, WHC-SD-WM-RPT-229 Rev. 0, September 1996.

Perry 1973, Chemical Engineers Handbook, Fifth Edition, 1973.

Powell 1995, Internal Memo 71210-95-005, Concentration of Low-Level Waste (LLW) Feed Using the PREDICT Model, March 23, 1995.

Powell et al. 1996, Neutralized Current Acid Waste Consolidation Management Plan, WHC-SD-WM-ER-532 Rev. 0, January 1996.

RHO 1980, Hanford High-Level Defense Waste Characterization - A Status Report, RHO-CD-1019.

RHO 1985, Hanford Defense Waste Disposal Alternatives: Engineering Support Data for the HDW-EIS, RHO-RE-ST-30P.

Rapko et. al. 1995, Washing and Caustic Leaching of Hanford Tank Sludges: Results of FY 1995 Studies, TWRSP-95-021, June 1995.

Schulz et. al. 1995, In-Tank Processes for Destruction of Organic Complexants and Removal of Selected Radionuclides, WHC-SD-WM-ES-321, April 1995.

- Shelton 1994a, Shelton to Garfield, Revised Inventory Estimates of Chemical and Radionuclides in Single- and Double-Shell Tanks, Internal Memo 71320-94.016, December 8, 1994.
- Shelton 1994b, Shelton to Higley, Estimated Chloride Inventory of Hanford Tank Waste, August 30, 1994.
- Shelton 1995a, Shelton to Kupfer, Double Shell Tank Inventories, Internal Memo 71320-95-003, February 24, 1995.
- Shelton 1995b, Shelton to Cooney, Radionuclide Inventory for Single- and Double-Shell Tanks, Internal Memo 71320-95-002, February 14, 1995.
- Shelton 1996, Projected Double-Shell Tank Supernate Composition and Inventory for Phase I Privatization, SD-WM-TI-751 Rev. 0, May 1996.
- Slaathaug, E. J., W. A. Peiffer, and K. D. Boomer 1995, Determine Waste Separations Process Trade Study, WHC-SD-WM-ES-356 Rev. 0, August 1995.
- Spells 1995, Transactions of the Institute of Chemical Engineers, 33, 79-84, 1955.
- Temer et. al. 1995, Sludge Washing and Alkaline Leaching Tests on Actual Hanford Tank Sludge: A Status Report, LAUR-95-2070, June 1995.
- Varma et. al. 1988, Identification of Glass Compositions Suitable for Disposal of Waste Reactive Metal, ANL-88-39, DOE/HWP-70, Argonne National Lab.
- WHC 1996, Tank Waste Remediation System Functions and Requirements Document, WHC-SD-WM-FRD-020, Rev. 0, March 1996.
- Wilson et. al. 1995, Melter Technology Evaluation for Vitrification of Hanford Site Low-Level Wastes, WHC-SA-2857-FP, April 1995.

Attachment 1

Note: the following table will be filled in with current numbers when they are available from Certa and Manuel.

Table 3-1a Phase I Chemical Feed

Component	LAW			HLW		
	Soluble (kg)	Insoluble (kg)	Total (kg)	Soluble (kg)	Insoluble (kg)	Total (kg)
Total Mass Flow						
Al(OH) ₄ ⁻						
Al ⁺³						
Bi ⁺³						
Ca ⁺²						
Cancrinite						
Ce ⁺³						
Cl ⁻						
CO ₃ ⁻²						
Cr(OH) ₄ ⁻						
Cr ⁺³						
Cs ⁺						
F ⁻						
Fe ⁺³						
H ₂ O						
La ⁺³						
Mn ⁺⁴						
Na ⁺						
Ni ⁺³						

N02-						
N03-						
OH-						
P04-3						
Si+4						
S04-2						
Sr+2						
Tc04-						
TOC						
U02+2						
Zr02:2H2O						

Table 3-1b Phase 1 Radionuclide Feed^{1,2,3}

Radionuclides	LAW			HLW		
	Soluble (Ci)	Insoluble (Ci)	Total (Ci)	Soluble (Ci)	Insoluble (Ci)	Total (Ci)
Total Activity						
Am-241						
C-14						
Cs-137						
Ba-137						
Cm-244						
Np-237						
Pu-238						
Pu-239						
Pu-240						
Pu-241						
Sr-90						
Y-90						
Tc-99						

¹Radionuclides decayed to 12/31/99.

²Amounts are consistent with the 1995 Integrated Database.

³SST is from TRAC; DST is from tank analysis.

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